



Singh, E., Kumar, A., Mishra, R., You, S. , Singh, L., Kumar, S. and Kumar, R. (2021) Pyrolysis of waste biomass and plastics for production of biochar and its use for removal of heavy metals from aqueous solution. *Bioresource Technology*, 320(A), 124278. (doi: [10.1016/j.biortech.2020.124278](https://doi.org/10.1016/j.biortech.2020.124278))

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Deposited on 21 October 2020

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1 **Pyrolysis of Waste Biomass and Plastics for Production of Biochar and Its Use for Removal**  
2 **of Heavy Metals from Aqueous Solution**

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9 **Abstract**

10 **The aim of this work was to study the pyrolysis of waste biomass and plastics and use the**  
11 **produced biochar for the removal of heavy metals from aqueous solution.** The batch experiments  
12 of Fe, Ni, Cu, Cr, Cd and Pb with biochars and plastic chars were carried for determining the  
13 effects of various experimental parameters (feedstock, contact time, adsorbent dose, pH and  
14 pyrolysis temperature). The isothermal sorption models demonstrated that the sorption capacities  
15 of biochars are higher in comparison to the plastic chars. The maximum removal efficiency  
16 shown by biochars and plastic chars at pH 4 was 99.86% and 99.93%, respectively. Both the  
17 carbon materials are thereby recognized as an environment-friendly and efficient pollutant  
18 control material at various studied parameters.

19  
20 **Keywords:** Biochars; Plastic chars; Pyrolysis; Removal efficiency; Heavy metals

21

## 22 1. Introduction

23 Heavy metals emanating from various industries are perilous for wellbeing and life of the animal  
24 and human (Zou et al., 2016). In the past few years, industrial growth has introduced massive  
25 pollutant levels in the water bodies. Due to their bioaccumulative and toxic nature, heavy metals  
26 have become a major concern. Substantial pollution of heavy metals in river bodies may be  
27 caused either by natural processes, such as flooding, weathering, or by human activities like  
28 waste disposal, industrial processes, or mining (Kaushik et al., 2009). The wastewater streams  
29 typically incorporate nickel (Ni), copper (Cu), chromium (Cr), cadmium (Cd), lead (Pb) and  
30 many more metals. They are non-biodegradable, and their concentrations regularly prompt  
31 bioaccumulation in living beings, causing health issues in human beings, animals and plants  
32 (Argun et al., 2007). For example, intemperate entry of Cu prompts extreme mucosal  
33 disturbance, hepatic damage and aggravation in the nervous system (Rehman et al., 2017). As  
34 indicated by an examination directed by the Central Water Commission (CWC, 2018), India's  
35 42 rivers have at least two heavy metals beyond the safe limit. Ganga, the National river of India,  
36 was found to be contaminated with five heavy metals (i.e. iron (Fe), Ni, Cu, Cr, and Pb). Other  
37 rivers like Arkavathi, Orsang, Rapti, Sabarmati, Saryu and Vaitarna were found to have even  
38 higher concentrations of these metals. The highest concentration of six major heavy metals found  
39 in Indian river as reported was Cd (0.07 mg L<sup>-1</sup>), Cr (0.45 mg L<sup>-1</sup>), Cu (0.31 mg L<sup>-1</sup>), Pb (0.37  
40 mg L<sup>-1</sup>), Ni (0.25 mg L<sup>-1</sup>) and Fe (14.56 mg L<sup>-1</sup>) (CWC, 2018). In India, major developmental  
41 activities depend on rivers, thereby making it very important to systematically study the removal  
42 techniques of heavy metals from water bodies (Kaushik et al., 2009).

43  
44 Recently, there has been a high demand for sustainable solution to tackle the problem of river  
45 contamination due to heavy metals. Many traditional techniques including membrane filtration,

46 electrochemical treatment, reverse osmosis, precipitation, ion exchange, electrodialysis and  
47 adsorption were employed to extract metal ions from wastewater. Although most of these  
48 techniques suffer from high overhead and capital expenses, adsorption is far better option  
49 because of its versatility in design, ease of handling and operation. At the same time, it is also  
50 considered more effective and economical ([Ahmadi et al., 2014](#); [Han et al., 2013](#)). From past  
51 few years, a considerable interest has been shown towards utilizing carbon and related materials  
52 as low-cost adsorbents for wastewater treatment ([Kumar et al., 2020a](#); [Singh et al., 2020](#)).

53 Heavy metal ions can be easily adsorbed by carbon materials because of their tunable surface  
54 functional groups. Existing studies have affirmed carbon materials as successful adsorbent of  
55 metal particles ([Sun et al., 2014](#); [Tounsadi et al., 2016](#)). Char is a typical type of carbon-rich  
56 material and could be generated by the thermo-chemical processing (e.g., pyrolysis and  
57 carbonization) of biomass or carbonaceous waste under an oxygen-deficient condition. It has  
58 been prepared from different feedstocks like plastic waste, wood, forest and farming residues  
59 which are capable of adsorbing substantial metals ([Inyang et al., 2016](#); [Johari et al., 2016](#)). The  
60 heavy metals sorption capacity of char is generally determined by the physico-chemical  
61 properties (e.g., specific surface area and surface functional groups) of char which are affected  
62 by the types and composition of feedstock as well the conditions of thermo-chemical processes  
63 ([Son et al., 2018](#)).

64  
65 There have been limited studies on comparing the adsorption performance of heavy metals and  
66 the underlying mechanism of char derived from organic origin (e.g., biomass) with that from  
67 synthetic origin (e.g., plastic waste). The former is referred as biochar while the latter is plastic  
68 char in this work. Singh et al. ([2020](#)) synthesized low-cost plastic char using Polyethylene (PE),  
69 Polyethylene terephthalate (PET) and Polyvinyl chloride (PVC) waste plastics and investigated

70 the effects it shows towards the sorption of arsenic. It was found that plastic chars also have  
71 prospects for usage as a sustainable adsorbent material and proficient removal of pollutants from  
72 aqueous media. Kumar et al. (2020a) concluded that the chars derived from organic origin i.e.  
73 biomass materials were suitable for effective sorption of the volatile organic compounds (VOCs)  
74 with the mechanism of physical sorption and partitioning. However, the intake capacity differed  
75 with the changing VOC types. A comprehensive review by Yang et al. (2019) on various carbon  
76 sorbents clearly stated the role of their functional groups towards the exceptional removal  
77 efficiency of heavy metals from the aqueous solutions by enhancing the surface properties and  
78 structural stability of the sorbent materials.

79  
80 This work deals with the use of two major carbon materials prepared from biomass and plastics  
81 towards purification of water bodies. It aimed to explain the role of these sorbents concerning  
82 their application for effective uptake of heavy metals from the polluted aqueous media. This  
83 work compared the compositions (proximate and ultimate), surface functional groups and surface  
84 morphology of biomass-derived chars (i.e. biochars) and plastic-derived chars (i.e. plastic chars).  
85 The metal ions uptake capacities between both the chars were also investigated in the current  
86 study. Although much work has been carried out using biochar towards the sorption of heavy  
87 metal ions, the use of chars derived from synthetic origin for the same remains understudied. The  
88 adoption of sustainable method for conversion of plastic and biomass wastes to chars for use as  
89 sorbent towards sorption of heavy metals as well as safeguarding the increasing loads of these  
90 waste warrant the present study.

## 91 **2. Materials and Methods**

### 93 **2.1 Materials**

94 Three biomass materials namely bamboo, sugarcane and neem were used for preparing biochar.  
95 The plastic char was prepared using PET, PE and PVC plastics. The biomass materials as well  
96 as plastic samples were washed, dried and then grinded using a mechanical grinder prior to  
97 pyrolysis. Pyrolysis was done using a fixed bed reactor comprising of a holder for placing the  
98 feedstock, a flow meter, gas collector, liquid collector and a water condenser. Moderate pyrolysis  
99 was performed in the presence of nitrogen (N<sub>2</sub>) at a flow rate of 1 L min<sup>-1</sup> at 450 °C and 550 °C  
100 at 8 °C min<sup>-1</sup> of heating rate to convert each feedstock of 60 g of into char. The final temperature  
101 was held for 10 min, similar to that of Singh et al. (2020). The char was then sieved to achieve  
102 0.5-1.0 mm size and dried at 105 °C for 18 hr and this was used for any further analysis. Both the  
103 chars were prepared in similar pyrolysis setups as followed in the previous works done by  
104 Kumar et al. (2020a, b) and Singh et al. (2020). The chars were named based on varying raw  
105 material, pyrolysis temperature and their applied dose for sorption as presented in **Table 1**.

106  
107 **Table 1**

## 108 **2.2 Characterization**

109 Fourier transform infrared (FTIR) spectroscopy, BET (Brunauer-Emmett- Teller) surface area  
110 analyzer and Scanning Electron Microscopy (SEM) images were used to characterize biochar  
111 and plastic char. The thermogravimetric (TGA) analyzer (Model: DTG 60, PerkinElmer, USA)  
112 was used to assess thermogravimetric properties such as thermal stability and changes in weight  
113 with changing temperature. The elemental analyses of the char were done using Elemental  
114 Analyzer (Model: CHNS 628, Leco, UK). The SEM images were captured using Scanning  
115 Electron Microscope (Model: Vega 3, Tescan, Czech Republic). The FTIR analysis was done  
116 using FTIR spectrometer (Model: Vertex 70, Bruker, USA) at a room temperature for  
117 determining the functional groups on the prepared char's surface. The specific surface area of the

118 chars was determined using BET surface area analyzer (Model: Autosorb iQ<sub>3</sub>, Quantachrome  
119 Instruments, USA) (Ladavos et al., 2012).

### 120 **2.3 Batch Sorption of Heavy Metals**

121 The batch sorption experiments of Fe, Ni, Cu, Cr, Cd and Pb with biochars and plastic chars  
122 were carried out in polypropylene tubes by batch technique for determining the effects of various  
123 parameters (contact time, adsorbent dose, pH and pyrolysis temperature). This was done by  
124 spiking Etalonmulti-element stock solution (Make: VMR Chemicals). Chars were prepared at  
125 two varying pyrolysis temperatures (450 and 550 °C). The solution was applied with 0.1 g and  
126 0.5 g of char and the solution pH was held at 4.0, 6.0 and 8.0 for a time range of 5 min to 35 min  
127 (contact time). A 20-ppm working solution was used for setting the experiment, and solution pH  
128 was balanced using hydrochloric acid (HCl) and sodium hydroxide (NaOH). Different  
129 concentrations of these metals were taken at room temperature for evaluating the isotherms. The  
130 suspensions were shaken for varying time (5, 10, 15, 20, 25, 30, 35 minutes) to achieve  
131 equilibrium state and the solid was then separated using 0.45 µm syringe filters. Inductively  
132 Coupled Plasma-Optical Emission Spectrometer (Model: iCAP 6000 Series, Thermo Scientific,  
133 USA) was then used to analyze the heavy metal ions present in sample. A blank solution without  
134 adding the char put as a control, which corresponded to zero loss of heavy metals during the  
135 analysis. Each experimental set was performed in triplicates to reduce the error chances. The  
136 difference between the initial concentration ( $C_0 \text{ mol L}^{-1}$ ) and the equilibrium one ( $C_e \text{ mol L}^{-1}$ )  
137 gave the adsorption percentage of ions.

### 138 **2.4 Isotherm Study**

139 Adsorption isotherm modelling is of fundamental importance while designing sorption-based  
140 system as they specify in what manner metals are partitioned between the aqueous medium and

141 the solid adsorbent as a function of concentration of the metal. When the char comes in contact  
 142 with the liquid solution, concentration of metals on the surface of adsorbent will increase until  
 143 the equilibrium is reached where there is an equal distribution of ions between solid-liquid phase.  
 144 Initial ion concentration was fixed at 20 mg L<sup>-1</sup> with two different doses (0.1g and 0.5g) of chars  
 145 at three pH value cases (4, 6 and 8). The heavy metals sorption was calculated using the least  
 146 squares regression approach. Langmuir isotherm's linear form is mentioned in equation 1

147 (Miandad et al., 2018):

148 
$$C_e/q_e = C_e/q_m + 1/k_L q_m \dots\dots\dots (1)$$

149 Where, q<sub>e</sub> (mg g<sup>-1</sup>) is the amount of sorbed metal ions, C<sub>e</sub> in (mg L<sup>-1</sup>) is the metal absorption at  
 150 equilibrium stage while q<sub>m</sub> (mg g<sup>-1</sup>) is the maximum uptake capacity of char and K<sub>L</sub> is the  
 151 Langmuir constant.

152  
 153 **2.5 Kinetic Study**

154 For determining the adsorption kinetics of the metals considered in the study, the kinetic  
 155 parameters were studied for time ranging from 5 min to 35 min by periodically checking the  
 156 percent elimination of the heavy metals. The obtained results were finally equated in Lagergren  
 157 equation that represents a first order kinetic equation (2) and a pseudo-second order kinetic  
 158 equation (3). The rate of heavy metals sorption on the char was calculated using pseudo-first-  
 159 order equation (2) (Jazini et al., 2017):

160 
$$\log(q_e - q_t) = \log q_e - (k_1 t / 2.303) \dots\dots\dots (2)$$

161 Pseudo-second-order equation (3) is of the form as per the equation (3) (Jazini et al., 2017):

162 
$$t/q_t = (1/k_2 q_e^2) + t/q_e \dots\dots\dots (3)$$

163 Where, q<sub>e</sub> and q<sub>t</sub> (mg g<sup>-1</sup>) signifies the metal ions sorbed at equilibrium and time t, whereas k<sub>1</sub>  
 164 and k<sub>2</sub> signifies the rate constants.



### 165 3. Result and Discussion

#### 166 3.1 Biochars and Plastic Chars Characterization

167 The data obtained from the proximate and elemental studies of the both chars (biochar and  
168 plastic char) are presented in Table 2. It is shown that the MC of biochars ranged from 0.36 wt.%  
169 to 2.15 wt.% while that of plastic chars ranged from 0.57 wt.% to 8.11 wt.%. The initial MC of  
170 biochars feedstock material ranged from 0.18 wt.% to 0.25 wt.%, while that of plastic chars  
171 feedstock material lied in between 0.60 wt.% to 2.01 wt.% ([Kumar et al., 2020a](#); [Singh et al.,  
172 2020](#)). The MC of the plastic chars was found to increase with higher pyrolysis temperature (550  
173 °C), while it decreased with increasing pyrolysis temperature in the case of biochars. The FC was  
174 found to be higher in bamboo-based biochar (85.4 wt.%) in comparison to that of plastic char  
175 (83.3 wt.%). The elemental analyses of the biochar showed lower content of nitrogen (0.47 to 1.0  
176 wt.%) while the carbon content was found to be between 52.7 to 78.1 wt.%. Jazini et al. ([2017](#))  
177 prepared barley straw-based biochar in similar range of pyrolysis temperatures (300 °C, 400 °C,  
178 500 °C) and found the nitrogen content ranging from 0.48 to 0.87 wt.% and carbon content from  
179 43.13 to 66.46 wt.%. The plastic chars showed 0.04 wt.% and 88.1 wt.% of nitrogen and carbon,  
180 respectively. With increasing pyrolysis temperature, an increase in the carbon content was  
181 observed, which is consistent with existing studies ([Fang et al., 2016](#); [Suliman et al., 2016](#)). On  
182 increasing the temperature from 350 °C to 600 °C, the carbon fraction was found to increase  
183 from 70.5% to 87.8%, 69.9% to 83.1% and 66.1% to 78.1% in the case of Douglas fir wood  
184 biochars, poplar wood biochars and Douglas fir bark biochars, respectively in the study  
185 performed by Suliman et al. ([2016](#)). The obtained results were also found to resemble that  
186 obtained elsewhere ([Wang and Liu, 2017](#)). In the present work, it was found that with the rise of  
187 temperature from 450 °C to 550 °C, the carbon content increased from 72.8 to 78.1 wt.% and

188 63.1 to 66.1 wt.% in neem-based char and bamboo char, respectively. On the other hand, the  
189 plastic chars showed consistent decrease in their respective carbon contents (54.6 to 36.8 wt.%,  
190 55.2 to 46.1 wt.% and 88.1 to 87.4 wt.% for PV, PE, PT chars, respectively) with the increasing  
191 pyrolysis temperatures.

192 **Table 2**

193 Plastic chars surface area ranged between 0.32-5.29 m<sup>2</sup> g<sup>-1</sup> while that of the biochar ranged  
194 between 1.04 - 43.9 m<sup>2</sup> g<sup>-1</sup>. The specific surface areas are affected by the types of feedstock and  
195 pyrolysis temperature. Sun et al. (2014) observed in their study that the surface area of bamboo  
196 char increased from 1.3 to 10.2 m<sup>2</sup> g<sup>-1</sup> with a rise in temperature from 300 °C to 450 °C. The  
197 changes in feedstock type at fixed pyrolysis temperature also showed a similar rise in the surface  
198 area i.e. in bagasse 5.2 to 13.6 m<sup>2</sup> g<sup>-1</sup> while in bamboo, this was 1.3 to 10.2 m<sup>2</sup> g<sup>-1</sup>. In the present  
199 work, the neem-based biochar (NC 1) had the highest specific surface area (43.9 m<sup>2</sup> g<sup>-1</sup>) at 550  
200 °C pyrolysis temperature. It was found that the plastic char (PE1) had highest specific surface  
201 area of 5.29 m<sup>2</sup> g<sup>-1</sup> which is almost eight times less than the highest area found in the case of  
202 biochar (NC 1) thereby confirming that the biochar to be more appropriate for use as adsorbent.  
203 The results validated the dependency of changing surface areas of the prepared chars on the raw  
204 material (feedstock) used along with the pyrolysis temperature. As pyrolysis temperature  
205 increased, the increase in the surface area of the biochar is possibly because of the decomposition  
206 of organic matters like lignin & cellulose and the formation of vascular bundles, channel  
207 structures and micro pores (Zhao et al., 2017). The destruction of aliphatic alkyls and ester  
208 groups as well as exposure to the lignin and cellulose available in the biomass feedstock at high  
209 pyrolysis temperature leads to the increased surface area (Tomczyk et al., 2020).

210 At low pyrolysis temperatures i.e. below 500 °C, lignin is not transformed to polycyclic aromatic  
211 hydrocarbon which makes the char more hydrophilic. At higher temperatures (>650 °C), the char  
212 formed is thought to be more hydrophobic and thermally stable (Tomczyk et al., 2020). Also, at  
213 higher temperatures, the pore-blocking substances thermally crack which increases the externally  
214 accessible surfaces and the release of higher volatile matter helps in formation of more pores  
215 (Rafiq et al., 2016; Shaaban et al., 2014).

216  
217 The major functional group detected using FTIR showed that all the spectra obtained displayed  
218 powerful absorption band allocated to O-H bond at 3501 cm<sup>-1</sup> for BC 1, 3565 cm<sup>-1</sup> for PE 1 and  
219 3544 cm<sup>-1</sup> for PT 1 (Li et al., 2013; Ren et al., 2013). The peaks obtained at 1053 cm<sup>-1</sup> and 1557  
220 cm<sup>-1</sup> in NC 1 is due to C-OH and C-O-C bonds. Peak at 1100 cm<sup>-1</sup>, 1590 cm<sup>-1</sup>, 3400 cm<sup>-1</sup>  
221 indicates C-OH, C=C and -OH groups presence, which were also noticed in an earlier study  
222 conducted by Yang et al. (2016). New bands at 2359 cm<sup>-1</sup> and 2883 cm<sup>-1</sup> obtained for SC 1 have  
223 been given to symmetric and asymmetric CH<sub>2</sub> groups. The peaks obtained at 668, 1035, 871,  
224 1053, 1416, 1539 cm<sup>-1</sup> are given to the aromatic rings (Machado et al., 2011), C-H and C-H O-  
225 H vibration mode and bending mode, respectively (Liu et al., 2010). The peaks observed from  
226 the study can be correlated to those found on activated carbon and graphene oxide (Ren et al.,  
227 2013). It is shown that both biochar and plastic char contain oxygen containing functional groups  
228 and thus confirms the presence of adsorption sites for heavy metal ions (Miandad et al., 2018).

229  
230 The morphology of NC 1, SC 1, PV 1 and PE 1 chars was studied using SEM. Plastic char  
231 showed rough surface with several cracks having spongy pores. This confirms that the char  
232 contains mesopores which is consistent with the study by Miandad et al. (2018). The cracked  
233 structures with pores also confirm the amorphous structure of the formed chars. This was

234 consistent with the results of the study performed using activated carbon for decontaminating  
235 copper by Ren et al. (2013). The biochar on the other hand showed smooth surfaces and long  
236 cylindrical structures having longer diameter. Furthermore, they were found to be curved and  
237 entangled among themselves. The interrelation among the pores of these biochars also predict  
238 better sorption capacity in comparison to the plastic chars. Similar morphological structure was  
239 found in the study conducted by Shaaban et al. (2013) using rubber wood sawdust-based chars  
240 prepared at 300 °C and 700 °C pyrolysis temperature. BET, SEM, FTIR, proximate and ultimate  
241 study described the structure of all the prepared chars. This research offered a qualitative and  
242 quantitative explanation of pyrolysis for sorption of heavy metals on the basis of char quality,  
243 quantity and its pore structures. These analyzes require time, and the measurements are mostly  
244 conducted after cooling down, which could result in a change in the char structure. Therefore,  
245 more sophisticated methods are required for analyzing the char performance to save time and  
246 money. The factors primarily responsible for adsorption are the specific surface area, contact  
247 time, feedstock content and pyrolysis temperatures.

248

## 249 **3.2 Adsorption Studies**

### 250 **3.2.1 Influence of the Feedstock Material**

251 **Fig. 1** shows the uptake capacities of heavy metals of all the prepared biochars and plastic chars.

252 Adsorption capacity is influenced directly with the changes in the raw samples being used. This

253 happens due to the changing physico-chemical properties of the biomass and plastic samples.

254 These changes in the properties of the feedstock are further responsible for the varying sorption

255 performance for uptake of heavy metals. In the case of biochars, the highest sorption of Ni

256 (99.01%), Cu (91.60%), Cd (99.24%), Fe (10.95%) and Pb (95.52%) was shown by SC 11 while

257 Cr (99.06%) by BC 11. Meanwhile, in the case of plastic chars, the highest sorption of Ni

258 (43.32%) and Cu (90.96%) was shown by PV 11 while Cd (28.31%), Fe (4.0%), Pb (70.07%)  
259 and Cr (99.01%) by PT 11. The experimental data obtained fitted well for Langmuir isotherm in  
260 comparison to Freundlich isotherm. The value of correlation coefficient ( $R^2$ ) for Pb sorption on  
261 different feedstocks was found to be 0.99 in case of Langmuir isotherm which inferred that the  
262 sorption on these biochars and plastic chars is favorable in the studied conditions. Therefore,  
263 chars prepared from biomass feedstocks showed higher adsorption capacities for all the heavy  
264 metals considered when compared with the one prepared from synthetic plastics. In a study  
265 performed by Kongsuwan et al. (2009) using activated carbon from eucalyptus bark having  
266 specific surface area of approximate  $1240 \text{ m}^2 \text{ g}^{-1}$  showed merely  $0.45$  and  $0.53 \text{ mmol g}^{-1}$  of  $\text{Cu}^{2+}$   
267 and  $\text{Pb}^{2+}$  ions, respectively. Although the chars used in the present study are non-activated one  
268 still both plastic as well as biomass-based char clearly showed high removal efficiencies thereby  
269 confirming the positive role played as sorbent materials. Studies performed by various  
270 researchers showed the respective uptake sorption capacities of chars prepared at  $400$  to  $600 \text{ }^\circ\text{C}$   
271 pyrolysis temperature from varying feedstocks under similar conditions as in corn straw ( $12.5$   
272  $\text{mg g}^{-1}$  of Cu,  $11.0 \text{ mg g}^{-1}$  of Zn), hardwood ( $6.8 \text{ mg g}^{-1}$  of Cu,  $4.5 \text{ mg g}^{-1}$  of Zn), oak wood ( $0.3$   
273  $\text{mg g}^{-1}$  of Cd,  $3 \text{ mg g}^{-1}$  of Pb), pine bark ( $0.4 \text{ mg g}^{-1}$  of Cd,  $2.6 \text{ mg g}^{-1}$  of Pb), oak bark ( $5.4 \text{ mg g}^{-1}$   
274 of Cd,  $13.1 \text{ mg g}^{-1}$  of Pb) and rice husk ( $0.3 \text{ mg g}^{-1}$  of Cu), respectively (Inyang et al., 2016;  
275 Chen et al., 2011). This confirms the varying uptake capacities of each sorbent formed from  
276 different feedstock materials irrespective of similar conditions of preparing them (Wang et al.,  
277 2019a). The obtained results in comparison with earlier studies confirmed the proficiency of the  
278 formed chars in efficiently removing heavy metals.

279 **Fig. 1.**

280

### 281 3.2.2 Influence of Pyrolysis Temperature

282  
283 The chars obtained at 550 °C (NC 11, BC 11, SC 11, PV 11, PE 11, PT 11) exhibited a higher  
284 sorption ability in comparison to the chars pyrolyzed at 450 °C (NC 00, BC 00, SC 00, PV 00,  
285 PE 00, PT 00). The percentage of Cd removal using NC, SC, PV, PT was found to be 45.86%,  
286 98.36%, 7.89% and 3.97% which increased to 66.40%, 99.24%, 24.58%, 28.31%, respectively  
287 with increasing pyrolysis temperature. This could be attributed to the lower specific surface areas  
288 of the char prepared at the lower temperature (450 °C). Wang et al. (2019b) reported a  
289 subsequent decrease in Cd removal efficiency using maize straw biochar from 97.1±0.8% to  
290 90±2% at 500 °C and 600 °C pyrolysis temperatures, respectively. The uptake efficiency of all  
291 the chars used in the present study showed increased removal efficiency with increasing  
292 pyrolysis temperature. Among all the chars studied, SC showed the maximum increase in uptake  
293 efficiency of Cd ions from 98.36% to 99.24% on increasing the temperature from 450 °C to 550  
294 °C. This shows the outstanding uptake efficiency of the prepared char in comparison to those  
295 reported in earlier studies (Wang et al., 2019b). Also, the results are noteworthy keeping in  
296 mind that the chars in the present study have not been modified by any means. The uptake  
297 capacities at different pyrolytic temperature of all the chars have been shown in **Fig. 2**. Analysis  
298 of Variance (ANOVA) was performed for studying the influence of different pyrolysis  
299 temperature on sorption capacity. The *p* value ( $2.2 \times 10^{-5}$  for 450 °C,  $3.4 \times 10^{-6}$  for 550 °C) obtained is  
300 very less than 0.05 thereby strongly confirming the rejection of null hypothesis. This low *p* value  
301 simply indicated the strong relationship between pyrolysis temperature (450 °C and 550 °C) and  
302 adsorption capacity.

303 **Fig. 2**

304

### 305 3.2.3 Influence of Char Dosage

306  
307 **Fig. 3** clearly showed that the adsorption of all the metals increased with an increase of char  
308 dosage from 0.1 to 0.5 g. All the other parameters i.e. pH, contact time, and temperature were  
309 kept constant for studying the effect of changing dosage of different chars on sorption capacity  
310 of heavy metals. Sorption of heavy metal ions was found to increase from 11.76 to 99.24%,  
311 87.62 to 99.36%, 36.43 to 91.59%, 0.60 to 10.95%, 11.56 to 43.31% and 59.0 to 95.52% for Cd,  
312 Cr, Cu, Fe, Ni and Pb, respectively on rising the dose from 0.1 g to 0.5 g. The obtained results  
313 confirm inter-relationship between the dose of char and removal capacity and subsequent  
314 increase in the available sorption sites. The surface area increases with an increase in the dose of  
315 char, which subsequently increases the free sites available for sorption. This is possibly the  
316 reason behind increased sorption capacity of the prepared char. Kula et al. (2008) reported a  
317 change in sorption capacity of the char with the change in its dose and also reported maximum  
318 removal of Cd<sup>2+</sup> at equilibrium time of 60 min, pH 6.0 and adsorbent dose of 1.0 g 50 mL<sup>-1</sup>.  
319 Acharya et al. (2009) also obtained 97.74% maximum removal of Pb<sup>2+</sup> at sorbent dose of 5g L<sup>-1</sup>,  
320 while the char studied in the present work showed a maximum of 99.36% removal with  
321 increased dose. This confirms the quality and presence of high specific area of the char prepared  
322 in this study.

323 **Fig. 3**

### 324 3.2.4 Influence of pH

325  
326 The variation in removal efficiencies of heavy metal ions by biochar and plastic char with  
327 respect to pH is shown in **Fig. 4**. The results clearly showed that the pH value significantly  
328 affects the removal efficiency of the char. At pH 4, the maximum removal was found to be

329 89.36%, 99.01%, 98.78%, 0.14%, 72.51% and 89.93% for Cu, Cd, Cr, Fe, Ni and Pb,  
330 respectively. The maximum removal efficiencies are 91.60% for Cu, 81.88% Ni, 95.52% Pb,  
331 99.24% for Cd, 99.03% for Cr and 4.81% for Fe at pH 6 which later decreased to 34.03%,  
332 72.10%, 58.64%, 61.07%, 49.08% at pH 8. Therefore, the removal efficiency of both the char  
333 was observed to increase with an increase in pH from 4 to 6. After pH 6, a significant decrease in  
334 the removal efficiency of the chars was observed. The influence of pH was also observed by  
335 Mousavi et al. (2010) while using waste tire rubber ash as an adsorbent to remove  $Pb^{2+}$  from  
336 waste stream. Mousavi et al. (2010) varied the pH from 4 to 6 and demonstrated that quantity of  
337  $Pb^{2+}$  ions uptake from solution rises rapidly from 73.8% at pH 4 to 93.1% at pH 6. Pellera et al.  
338 (2012) also reported maximum Cu (II) uptake of 93.6%, 90.1%, 88.7% and 77.8% at pH 7 by the  
339 biochars prepared from compost, rice husks, orange waste and olive pomace, respectively. The  
340 results from the previous studies as well as the present study clearly demonstrated that the metal  
341 ions are better removed at higher pH range. The carbon content found in any char material  
342 studied acts mostly as a weak alkali that buffers the pH of the working solution. After the rise in  
343 pH, it becomes more difficult for the heavy metal ions present in the sample solution or the  
344 aqueous media to dissolve as it becomes less soluble. This thereby allows the sorption of the  
345 positively charged toxic heavy metal ions to be easily on the surface of the adsorbent which is  
346 then removed from the polluted stream. All the aquatic media are in general quite sensitive to pH  
347 and thereby special care needs to be taken while treating them. Hence, a pH neither alkaline nor  
348 acidic in nature is generally considered as the best for proper remediation. In this study, pH 6 has  
349 been found as the best one for removing heavy metals concentration.

350 **Fig. 4**

351



### 352 3.2.5 Influence of Contact Time

353  
354 The sorption rate of Fe, Cu, Cd, Cr, Ni and Pb on all the chars regardless the carbon material  
355 used increased with change in the contact time. After the attainment of equilibrium condition at  
356 20 min, the adsorption rate decreases progressively due to the limited free spaces available. This  
357 is because the adsorption efficiency of metal ions on the char is rapid during the first stage (0 to  
358 20 min) for all the metal ions studied. The sorption rate also decreased after 20 min contact time  
359 and marginal changes occur till 35 min. Sorption of these metals onto the adsorbents (NC 11, PT  
360 11, NC 00 and PT 00) also showed increasing uptake with increasing time during initial stage (0-  
361 20 min). After this, rate decreased and the equilibrium state was attained after 20 min. This is  
362 mostly due to the availability of well aligned free spaces of char for binding together the toxic  
363 heavy metal ions. After this stage, the sorption capacity of the char slowly decreases until the  
364 equilibrium condition is reached because of the saturation of all the available sites. Also, for  
365 studying the kinetics, pseudo first and second order models were applied. It was found that  
366 pseudo second order model fits better in comparison to pseudo first order model. The  $R^2$  value in  
367 pseudo second order was 0.99. This confirms the that the sorption of heavy metals on both the  
368 chars is a chemical process. The obtained results were similar to those obtained from the  
369 experiment.

370 In adsorption experiment study conducted by Peller et al. (2012), the reduction of Cu (II) was  
371 accomplished by increasing the contact time. In most of the cases, a slower adsorption rate  
372 followed the rapid initial adsorption rate within the first few min before reaching equilibrium. It  
373 is because of presence of ample amount of available biochar site, while as adsorption proceeded  
374 the depletion of these active sites also occurred over time.

375

### 376 **3.2.6 Influence of Surface Area**

377 A correlation evaluation of specific surface area of biochars and plastic chars was performed to  
378 analyze the effect on adsorption capacity on the basis of obtained results (**Fig. 1**). None of the six  
379 metals produced a line graph when their respective sorption capabilities were considered, which  
380 differed from those of other carbon materials (**Kumar et al., 2020a**). The sorption took place in  
381 accordance to the adsorption-partitioning processes. The interaction between sorption and  
382 surface area indicated that the adsorption of metals by char produced at 550 °C is primarily  
383 exothermic. Also, it is compatible with the adsorption-partition cycle. In the case of biochars  
384 prepared at higher temperatures, i.e. 550 °C with higher surface area and lower non-carbonized  
385 organic matter, adsorption is the dominant mechanism while partitioning remains a mechanism  
386 for chars prepared at lower pyrolysis temperatures with lower surface area and higher non-  
387 carbonized organic matter (**Kumar et al., 2020a**).

### 388 **3.3 Statistical Analyses**

389 Heavy metals sorption was done using ANOVA to obtain the basic data about the efficacy of  
390 parameters set for the sorption. The influence of independent variables on the dependent ones i.e.  
391 pH and sorption were studied. The statistically significant values were symbolized as p-values. It  
392 was found to be 0.012 for all the chars applied on different pH which indicated a positive relation  
393 between the sorption capacity, pH (4.0, 6.0, and 8.0), dose (0.1 g, 0.5 g) and contact time (35  
394 min). F value was found to be 2.95 that is more than the F critical (2.21) for single way. This  
395 shows the rejection of null hypothesis and that the char dose plays a major role in its uptake  
396 capacity.

397

398

### 399 3.4 Isotherm Modeling and Kinetic Study

400 The data obtained from the sorption analysis were put to Langmuir adsorption isotherm using  
401 linear expression of the model similar to that used in the study performed by Miandad et al.  
402 (2018). The isotherm assumes homogenous surface and a continuous sorption potential. The  
403 sorption capacity of the biochar followed Langmuir isotherm with  $R^2$  value being 0.99, thereby  
404 confirming the process of sorption being chemical. The increase in the sorption capacity of the  
405 char with increase in metal ion concentration is because of the high concentration gradient that  
406 resists the mass transfer from aqueous media to solid char. After a certain time, the efficiency of  
407 uptake of ions does not increase because the number of available sites is fixed. Son et al. (2018)  
408 also found Langmuir isotherm to fit better in the sorption study performed using marine macro  
409 algae for the uptake of Cu, Cd and Zn ions. Li et al. (2013) also demonstrated Langmuir model  
410 to be more suitable in comparison to Freundlich model to the obtained sorption data. Langmuir  
411 isotherm stated that monolayer sorption took place. The Langmuir model predicts the suitability/  
412 favorability of the adsorption process to take place using both the chars. The linear form of the  
413 model suggests that the char prepared has high affinity towards the positively charged metal ions  
414 and would support the sorption process under the controlled experimental conditions. Biochars  
415 and plastic chars samples used in the present study presented moderately similar sorption by BC  
416 11 and PV 11 which implied that chemical and physical sorption is involved in the entire  
417 adsorption procedure. Metal ions, amount of carbon material used, pH, contact time are  
418 accountable for the percentage removal of these metal ions. Even though the chars showed  
419 moderate surface areas, but because of high oxygen, it showed sorption of the metal ions on pore  
420 surface (Mohan et al., 2014).

421

422 The kinetic data in the present study was done with the help of some models. The models were  
423 verified by the fitness check of the lines obtained. The  $R^2$  value clearly demonstrated that the  
424 data obtained during the study followed the retention kinetic of all the heavy metal ions. The first  
425 order kinetic model calculated  $q_e$  value differs from the experimental values and obtained  $R^2$   
426 values also. The calculated  $q_e$  values for second order model are somewhat near to the  
427 experimental value. The  $R^2$  value was more in the case of pseudo second order kinetic model.  
428 This confirms the suitability of pseudo-second order model for better explaining the sorption of  
429 metal ions on different plastic char and biochar sorbents used in the study. Also, this confirms  
430 chemisorption being the fundamental mechanism behind the sorption of heavy metal ions on the  
431 biochar and plastic char surface by exchange of valence electron between adsorbate and  
432 adsorbent. The positive results for the sorption of six heavy metals found in Indian river using  
433 biomass and plastic-based chars thus suggested that both these chars serve as alternative sorbents  
434 to mitigate the heavy metals contamination. Large-scale field experiments will be required to  
435 examine the effects of char-based sorbents on reducing the heavy metals concentrations in river.

## 436 5. Conclusion

437 The study focused on synthesis of carbon materials from biomass and plastic wastes and  
438 comparing their performance as an economical heavy metals sorbent. It revealed the dependency  
439 of various factors like dose, pyrolysis temperature, feedstock type, contact time and pH on the  
440 sorption capacity. SC biochar was found to be most effective with sorption efficiencies ranging  
441 from 3.27-99.4%. Although, some challenges need to be addressed while implementing  
442 purification of aqueous media using these materials, the performance shown by biochars  
443 favorably suggested their use for better results. Carbon materials are thereby a proved sustainable  
444 solution towards purification of river water.

445 **CRedit authorship contribution statement**

446 **Ekta Singh:** Conceptualization, Methodology, Investigation, Writing -original draft, Writing -  
447 review & editing. **Aman Kumar:** Conceptualization, Methodology, Investigation, Writing -  
448 original draft, Writing - review & editing. **Rahul Mishra:** Conceptualization, Investigation,  
449 Writing - original draft, Writing - review & editing. **Siming You:** Validation, Writing - review &  
450 editing. **Lal Singh:** Conceptualization, Validation. **Sunil Kumar:** Funding acquisition, Writing -  
451 review & editing, Supervision. **Rakesh Kumar:** Supervision.

452 **Declaration of Competing Interest**

453 The authors declare that they have no known competing financial interests or personal  
454 relationships that could have appeared to influence the work reported in this paper.

455 **Acknowledgments**

456 This research was supported through In-house R&D laboratory project of CSIR-NEERI. The  
457 authors gratefully acknowledge the support provided by the Director, CSIR-NEERI in  
458 completing the study.

459 **Appendix A. Supplementary data**

460 E-supplementary data for this work can be found in e-version of this paper online

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