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Molten Salt Synthesized Submicron Perovskite $\text{La}_{1-x}\text{Sr}_x\text{CoO}_3$ Particles as Efficient Electrocatalyst for Water Electrolysis

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Perovskite oxides are an important and effective class of mixed oxides which play a significant role in the fields of energy storage and conversion systems. Here we present a series of cobaltite perovskite LaCoO_3 particles which have been doped with 0, 5, 10, 20, and 30% of Sr^{2+} and have been synthesized by a combined sol-gel and molten-salt synthesis procedure, which provides a regular morphology of the particles. These Sr^{2+} -doped LaCoO_3 particles have been characterized by powder X-ray diffraction, Raman spectroscopy, infrared spectroscopy, X-ray photoelectron spectroscopy, and scanning electron microscopy. Moreover, these Sr^{2+} doped LaCoO_3 particles have been demonstrated as efficient catalysts for oxygen evolution reaction (OER) based on the measured specific capacitance, total charge, most accessible charge, electrochemically active surface area, and roughness factor using rotating disk and rotating ring-disk electrode techniques. The 30% Sr^{2+} -doped LaCoO_3 sample shows enhanced electrocatalytic OER activity in 0.5 M H_2SO_4 media compared to the LaCoO_3 samples doped with 0, 5, 10, and 20% Sr^{2+} . Among all five LaCoO_3 samples, the doped LaCoO_3 samples demonstrate better OER activity than the undoped sample.

Keywords: LaCoO_3 , sol-gel, molten-salt synthesis, electrocatalysis, OER, Sr^{2+} -doped

INTRODUCTION

Growing environmental and geopolitical problems have been arising from the shortage of fossil fuel, promoting efforts to develop cheap, ample, and eco-friendly materials for advanced energy conversion and storage systems. In water electrolysis, the overpotential requirement is a serious issue at which oxygen evolution reaction (OER) occurs (Huynh and Meyer, 2007; Yeo and Bell, 2011). Therefore, it is a significant challenge to design active electrocatalysts for water electrolysis to meet the demands of the sustainable energy-powered economy (Loi and Hummelen, 2013). On the other hand, the global use of noble metal oxides like ruthenium and iridium oxides, especially in the field of catalysis, requires us to minimize the use of these noble metal oxides and to introduce new types of materials, e.g., perovskite oxides. Perovskites are fascinating alternatives to noble metals because of their catalytic activity and cost-effectiveness (Gasteiger et al., 2005; Jörissen, 2006; Neburchilov et al., 2010).

Perovskite oxides have the general formula of ABO_3 , where A is lanthanide, alkaline-earth, or alkaline cations, and B is transition metal cations such as Fe, Mn, Co, Cr, or Ti. Perovskite

oxides can be customized with chemical and physical properties due to the exceptional tunability of their structure and composition. They are a type of mixed oxide and are a class of materials that show a remarkable electronic structure, redox behavior, ionic and electronic activity, and thermal stability (Pena and Fierro, 2001; Schaak and Mallouk, 2002; Royer et al., 2014; Zhu et al., 2014). Perovskites with multiple A or B cations of difference sizes and valences have distortion in their crystal structure. Doping of A or B cations of perovskite with elements of Ce, Ba, or Sr creates oxygen vacancies and increases oxygen mobility (Nitadori and Misono, 1985; Nitadori et al., 1986; de la Cruz et al., 2001; Mefford et al., 2014). In perovskites, the cations present on A and B sites play a crucial role in altering its electronic structure and tuning catalytic properties (JO'M et al., 1983; Bockris and Otagawa, 1984; Vojvodic and Nørskov, 2011; Mueller et al., 2015).

Due to their slow reaction kinetics, both OER and oxygen reduction reaction (ORR) need electrocatalysts. Pt and Pt-alloys are the most essential catalysts for ORR while the Ir and Ru-based materials are good OER catalysts (Gupta et al., 2009; Slanac et al., 2012; Cui et al., 2013; Mefford et al., 2016). Many research studies based on perovskites for OER and ORR have been focused on structural and electronic properties of the surface or bulk (Otagawa and Bockris, 1983; Bockris and Otagawa, 1984; Matsumoto and Sato, 1986). Over the past 40 years, La_{0.8}Sr_{0.2}CoO₃ has been studied to give different mechanistic theories as an active catalyst for ORR (Meadowcroft, 1970). For example, Hong et al. (2015) summarized the OER activity by showing correlations between the surface and bulk properties of metal oxides and their electrocatalytic activities. This study showed that the substitution of La²⁺ by Sr²⁺ to maintain the perovskite structure following the effects of vacancy defects, covalency, and oxygen exchange on the electrode surface during the electrocatalysis of OER. LSCO (LaSrCoO₃) electrocatalysis in alkaline media showed good structural stability, electrolytic corrosion resistance, and high activities for ORR and OER (Jasem and Tseung, 1979; Gorlin and Jaramillo, 2010; McCrory et al., 2013).

There are several procedures to synthesize Sr²⁺-doped LaCoO₃, such as solid-state synthesis (Li et al., 2002), sol-gel (Patel and Patel, 2012), chemical vapor deposition (CVD; Armelao et al., 2005), spray-freeze drying (Lee et al., 2006), aqueous gel-casting technique (Cheng et al., 2008), thermal decompositions (Kaituo et al., 2014), precipitation (Singh and Rakesh, 2009), combustion (Luo and Liu, 2007), low pressure plasma synthesis (Rousseau et al., 2007), etc. In terms of morphology control of products, many of these methods are not sufficient, including the solid-state route and sol-gel method. Molten-salt synthesis method is a simple, reliable, eco-friendly, and cost-effective method when compared to the methods mentioned above. To obtain undoped and Sr²⁺-doped LaCoO₃ particles with a controlled and regular morphology, we introduced a new combination of sol-gel and molten-salt synthesis procedure in this work. Furthermore, we studied their catalytic applications of OER.

Specifically, we successfully synthesized uniform LaCoO₃ particles with 0, 5, 10, 20, and 30% Sr²⁺ nominal doping levels

using our facile and reliable method. We characterized their composition, morphology, and structure by powder X-ray diffraction (XRD), Raman spectroscopy, infrared spectroscopy, X-ray photoelectron spectroscopy, X-ray energy dispersive spectroscopy, and scanning electron microscopy. More importantly, their electrocatalytic performance for OER in acidic 0.5 M H₂SO₄ media was investigated systematically using rotating disk and rotating ring-disk electrode techniques in terms of specific capacitance, total charge, most accessible charge, electrochemically active surface area, and roughness factor. The 30% Sr²⁺-doped LaCoO₃ sample showed the highest electrocatalytic OER activity compared to the LaCoO₃ samples doped with 0, 5, 10, and 20% Sr²⁺. Among all five LaCoO₃ samples, the doped LaCoO₃ samples demonstrate a better OER activity than the undoped sample. Therefore, this study proves that the combined sol-gel and molten-salt synthesis method is a novel and desirable method to prepare LaCoO₃ particles with a uniform morphology and enhanced OER activity in acidic media.

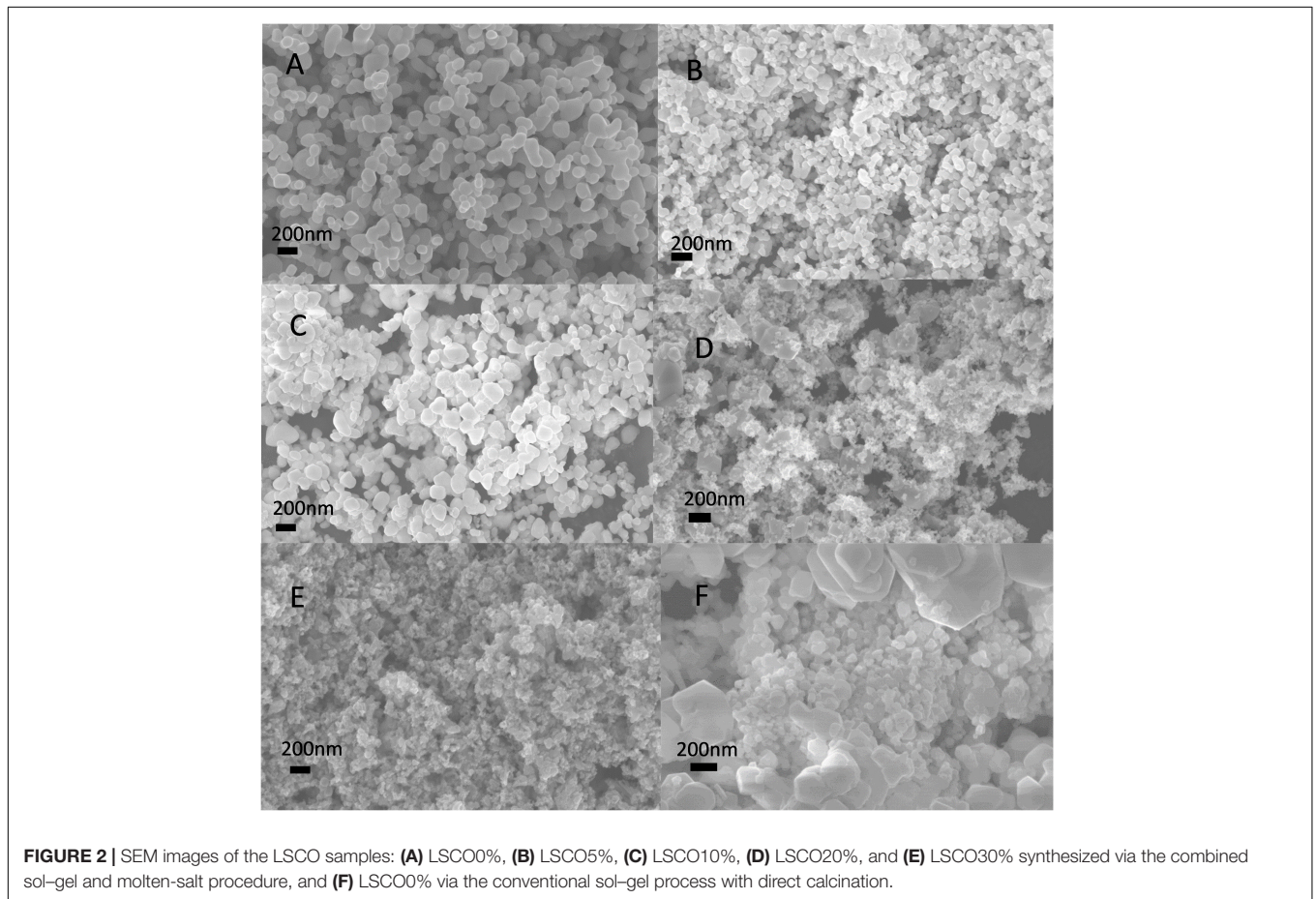
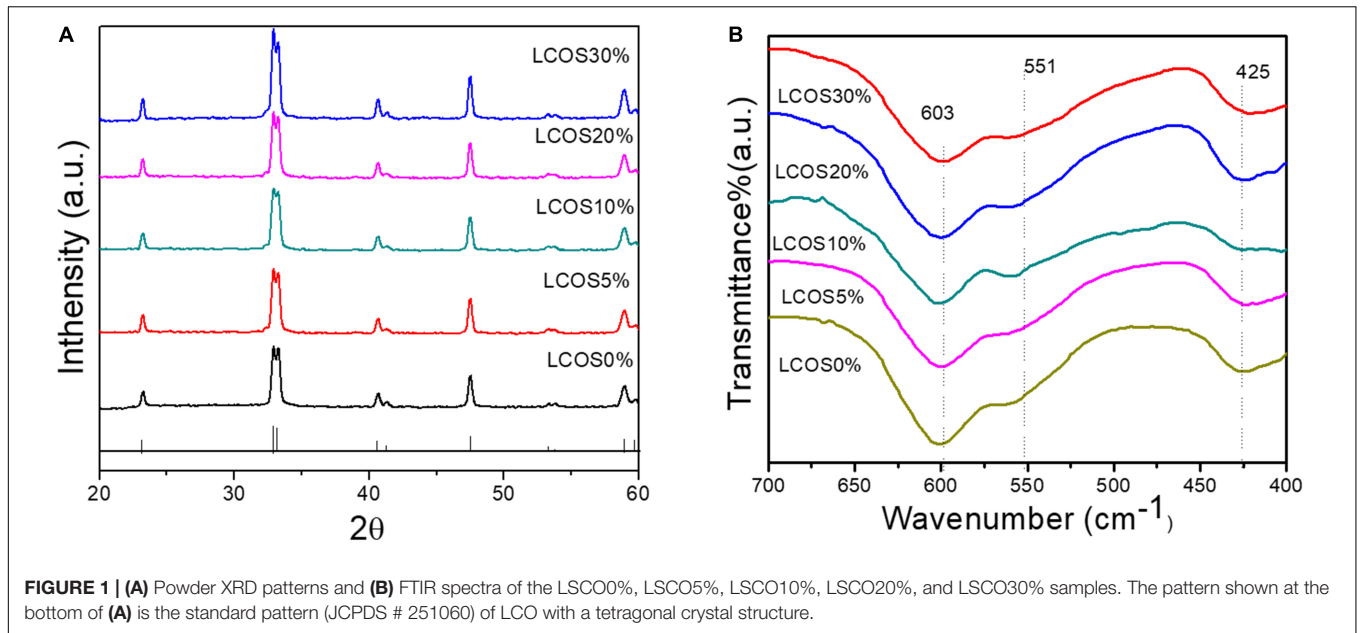
EXPERIMENTAL SECTION

Materials and Synthesis

The Sr²⁺-doped LaCoO₃ samples were prepared as follows using the combined sol-gel and molten-salt method synthesis process. Specifically, in a representative synthesis, a stoichiometric amount of La(NO₃)₃·6H₂O, Sr(NO₃)₃ and Co(NO₃)₂·6H₂O on a 1 mM scale were added into 10 ml distilled water. After stirring for 2 h at room temperature, polyvinyl alcohol (PVA) aqueous solution (20 wt%) was added. After further stirring, the obtained sol was dried in an oven at 80°C for 2 h, followed by 120°C on a hot plate overnight. During the molten-salt synthesis step, 0.23 g dried gel of each of the five samples was first mixed with 60 mM of NaNO₃ + KNO₃ mixture (1:1) and then ground together in a mortar and pestle for 20 min (Zuniga et al., 2018). The resulting mixture was transferred into a crucible and kept at 700°C for 6 h with a ramp-up rate of 15° min⁻¹ and cooling-down rate of 10° min⁻¹. In the final step, the annealed products were washed with deionized water several times and dried in an oven at 60°C overnight. The prepared LaCoO₃ samples doped with 0, 5, 10, 20, and 30% Sr²⁺ were denoted as LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30%, respectively.

Materials Characterization

The samples were characterized by powder XRD on a Rigaku-MiniflexTM II X-ray diffractometer with Cu K_{α1} radiation (λ = 0.15406 nm). The XRD data were collected using a scanning mode in the 2θ range from 20° to 80° with a scanning step size of 0.04° and a scanning rate of 4.0° min⁻¹. Raman scattering data was recorded by employing the back-scattering geometries on a Bruker SENTERRA RAMAN microscope with an objective of 20× of an optical microscope. The excitation line (785 nm) of an Ar+ laser beam was focused to a spot size of 5 μm with a laser power of 25 mW. The spectral resolution range used was 3–5 cm⁻¹ with an integration time of 100 s. Infrared spectra were recorded on a Thermal Nicolet Nexus 470 spectrometer. The morphology of the LSCO samples was observed by a field



emission scanning electron microscope (SEM, Carl Zeiss Sigma VP FESEM) equipped with a field emission gun operated at 5 kV.

Electrode Preparation and Electrochemical Measurement

Three-electrode electrochemical cell configuration was used (Mohan and Mao, 2018; Mao et al., 2019). The working electrode was the catalyst-coated glassy carbon electrode with an area of 0.5024 cm²; a platinum wire was used as the counter electrode and the Ag/AgCl electrode as the reference electrode. To prepare the working electrode, we first prepared the catalyst ink by dispersing 1 mg of the LSCO catalyst powder as active material in 362 μL water and 57 μL Nafion solution by sonication for 20 min. In the next step, we took 42 μL of the prepared catalyst ink, cast it onto the surface of the glassy carbon electrode which corresponds to 0.38 mg/cm², and dried it in a vacuum oven overnight. The electrochemical measurements, including cyclic voltammogram (CV) and linear sweep voltammogram (LSV), were performed in 0.5 N H₂SO₄(aq) electrolyte which was purged with nitrogen gas for 10 min prior to the electrochemical measurements to remove the dissolved air from the electrolyte toward the OER using an Autolab potentiostat/galvanostat (PGSTAT302) with Nova 10.11 software. Current density was evaluated as a function of applied voltage from the range of 0.4–1 V versus the Ag/AgCl at scan rates of 5, 10, 20, 50, 70, and 100 mV/s for CV characterization. Linear

sweep voltammogram was done at a scan rate of 5 mV/s for all five catalysts in terms of OER.

RESULTS AND DISCUSSION

Materials Characterization

Figure 1A shows the XRD patterns of the synthesized samples of LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30%. The observed reflections could be perfectly indexed with the peaks of (0 1 2), (1 1 0), (1 0 4), (2 0 2), (0 0 6) (0 2 4), (1 2 2), and (2 1 4) on the basis of tetragonal crystal structure (JCPDS file #251060). The XRD of all five catalysts were found to be crystalline in nature. In addition to XRD data, evidence regarding the chemical composition of the synthesized products was obtained from IR spectra (**Figure 1B**). The observed FTIR absorption band at ~603 cm⁻¹ could be assigned to the vibration of the Co–O bond in an octahedral coordination while the band observed at ~551 cm⁻¹ for La(Sr)–O bond stretching. Furthermore, the vibration of the La–O bond in a dodecahedral coordination was confirmed by the presence of a strong peak at 425 cm⁻¹ (Khalil, 2003; Mahmood et al., 2013; Agilandeswari and Ruban Kumar, 2014).

SEM images of the as-synthesized LSCO samples show the formation of submicron globules as first reported for LSCO (**Figures 2A–E**). We also prepared a LSCO0% sample by

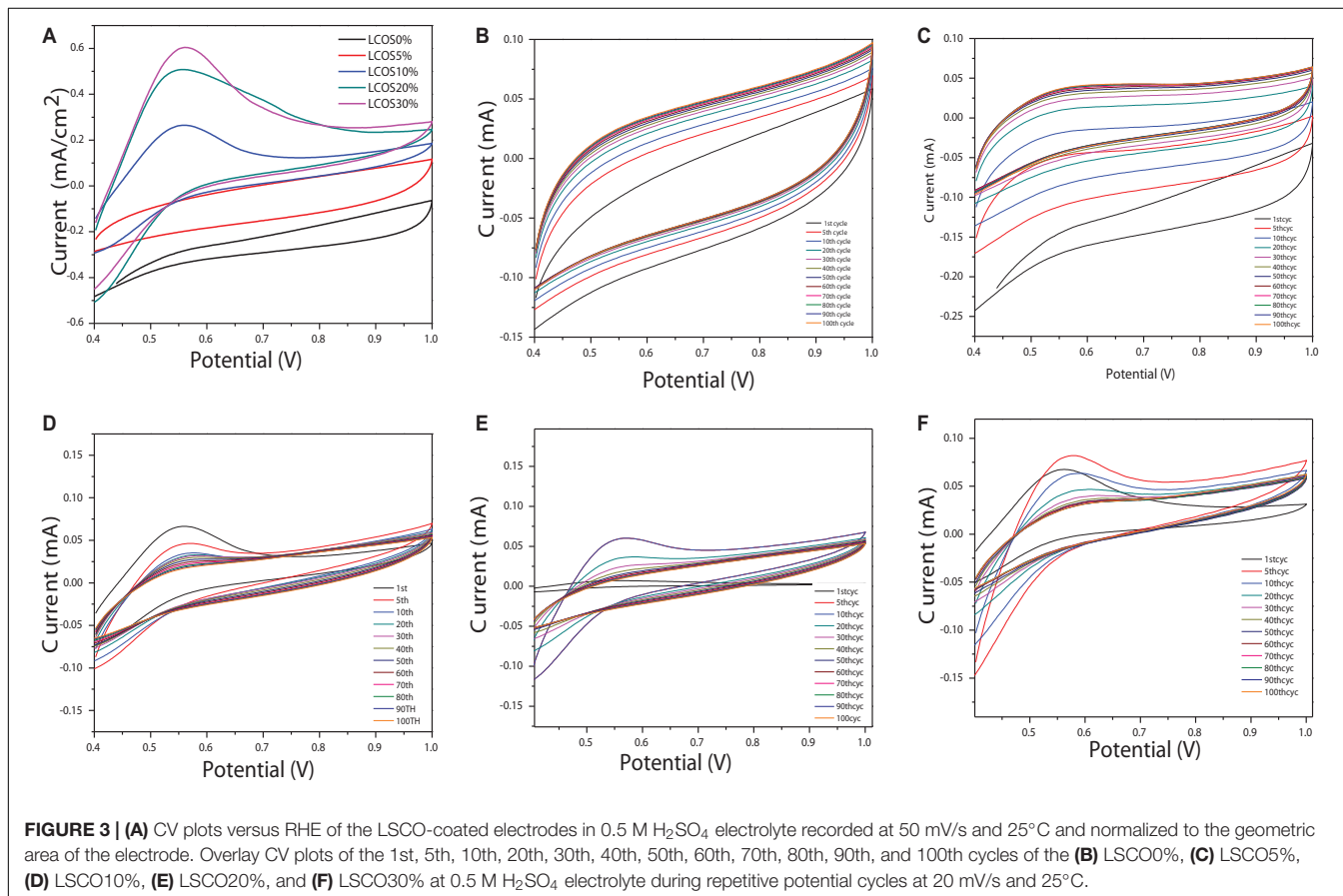


TABLE 1 | Calculated specific capacitance of the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples at scan rates of 5, 10, 20, 50, 70, and 100 mV/s.

Scan rate (mV/s)	Specific capacitance (F/g)				
	LSCO0%	LSCO5%	LSCO10%	LSCO20%	LSCO30%
5	0.013285	0.096237	0.202794	0.216114	0.153646
10	0.113586	0.756654	1.054873	1.077412	0.809768
20	0.095984	0.455375	0.562605	0.555099	0.425452
50	0.054455	0.215751	0.257138	0.235581	0.186782
70	0.040588	0.165006	0.193801	0.174456	0.122107
100	0.036369	0.127018	0.143689	0.130235	0.074329

TABLE 2 | Voltammetry charges (q^*) of the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples at scan rates of 5, 10, 20, 50, 70, and 100 mV/s.

Scan rate (mV/s)	q^*				
	LSCO0%	LSCO5%	LSCO10%	LSCO20%	LSCO30%
5	0.010637	0.115024	0.242383	0.258304	0.18364
10	0.013576	0.090437	0.12608	0.128774	0.096785
20	0.011472	0.054427	0.067244	0.066346	0.050851
50	0.006509	0.025787	0.030734	0.028157	0.022325
70	0.004851	0.019722	0.023164	0.020851	0.014594
100	0.010637	0.015181	0.017174	0.015566	0.008884

TABLE 3 | Comparison between the total charge, outer charge, and charge accessibility of the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples.

Catalyst	q^*_{total} (mC)	q^*_{outer} (mC)	Accessibility (q^*_{outer}/q^*_{total})
LSCO0%	33.6	0.002625	0.000078
LSCO5%	5.474	0.0057	0.00104
LSCO10%	4.68	0.01567	0.0033
LSCO20%	1.4160	0.0206	0.0145
LSCO30%	0.765	0.00932	0.0128

direct calcination of the sol-gel precursor (i.e., the dry gel was not treated with the molten-salt process) for comparison. As commonly observed from samples synthesized by the sol-gel process, the obtained LSCO0% product shows an irregular morphology and larger particles (Figure 2F). Therefore, in terms of product morphology, these SEM images confirm that our combined sol-gel and molten-salt synthesis process is better than the conventional sol-gel process.

Electrochemical Characterization

The CV curves of all LSCO catalysts modified as working electrodes (Figure 3A) exhibits a characteristic shape with the presence of the anodic and cathodic peak at a potential range of 0.4–1 V vs reversible hydrogen electrode (RHE), indicating a nonreversible reaction (Mohan and Mao, 2018; Mao et al., 2019). Also, the LSCO30% sample showed the highest current density and the LSCO0% showed the lowest current density among the five samples.

To find out charge accumulation at the electrode/catalyst interface and to evaluate electrode capacity, capacitance measurements were conducted. The two electrochemical

contribution faradic and proton adsorption processes are not integrated at the chosen potential range from 0.4 to 1 V. To avoid faradic contribution, we calculated specific capacitance (C , F/g) here for all LSCO catalysts by integrating the CV curves between 0.4 and 1 V vs RHE at scan rates of 5, 10, 20, 50, 70, and 100 mV/s using Eq. 1:

$$C = \frac{1}{\gamma m (E_2 - E_1)} \int_{E_1}^{E_2} i(E) dE \quad (1)$$

where γ is the scan rate (V/s), m is the mass in grams of the catalyst deposited on the working electrode, E_1 and E_2 are limits of potentials of the integration curves, and $\int_{E_1}^{E_2} i(E) dE$ is the integration of the CV curve. From the calculated specific capacitance values tabulated in Table 1, we can see that the capacitance values decrease for all five LSCO catalysts with an increasing scan rate. This observation indicates that the double layer formation is more consistent in a quasi-stationary mode (Sugimoto et al., 2006; Devadas et al., 2011). The diffusion of active species can occur even in miniature pores, thereby all of the active sites of the LSCO samples contribute to the double layer formation. However, at a high scan rate, the charge accumulation occurs only on the active surface sites. The diffusion effect limits the migration of electrolytic ions and causes some active surface areas to be inaccessible for charge storage.

The calculated specific capacitance values of the LSCO0% and LSCO5% samples are lower than those obtained for the LSCO10% and LSCO30% samples, while those from the LSCO20% sample showed the highest values. Overall, the specific capacitance values of our LSCO samples are in the order of LSCO20% > LSCO30% > LSCO10% > LSCO5% > LSCO0%. Specific capacitance indicates the stability of the catalysts

on the electrode surface or due to morphology change making the catalysts less accessible to charges (Ardizzone et al., 1990). The increase of capacitance can also be correlated to the higher oxidation state of metallic ions in metal oxides (Ardizzone and Trasatti, 1996). Therefore, to improve the charge accumulation, it is important to increase the number of active sites and their accessibilities. For our LSCO samples, the presence of a well-defined morphology and the miniature size of the formed submicron particles refers to the high concentration of active sites at the electrolyte/catalyst interface with a large oxidation state change, and therefore improved capacitive properties (Mohan and Mao, 2018).

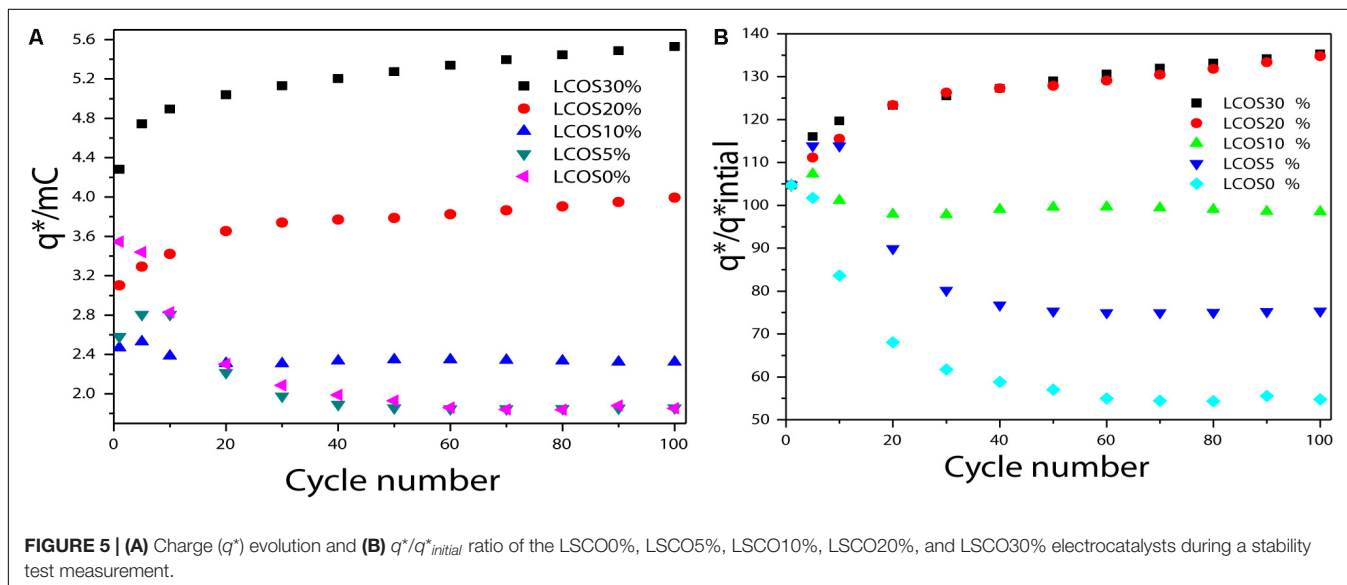
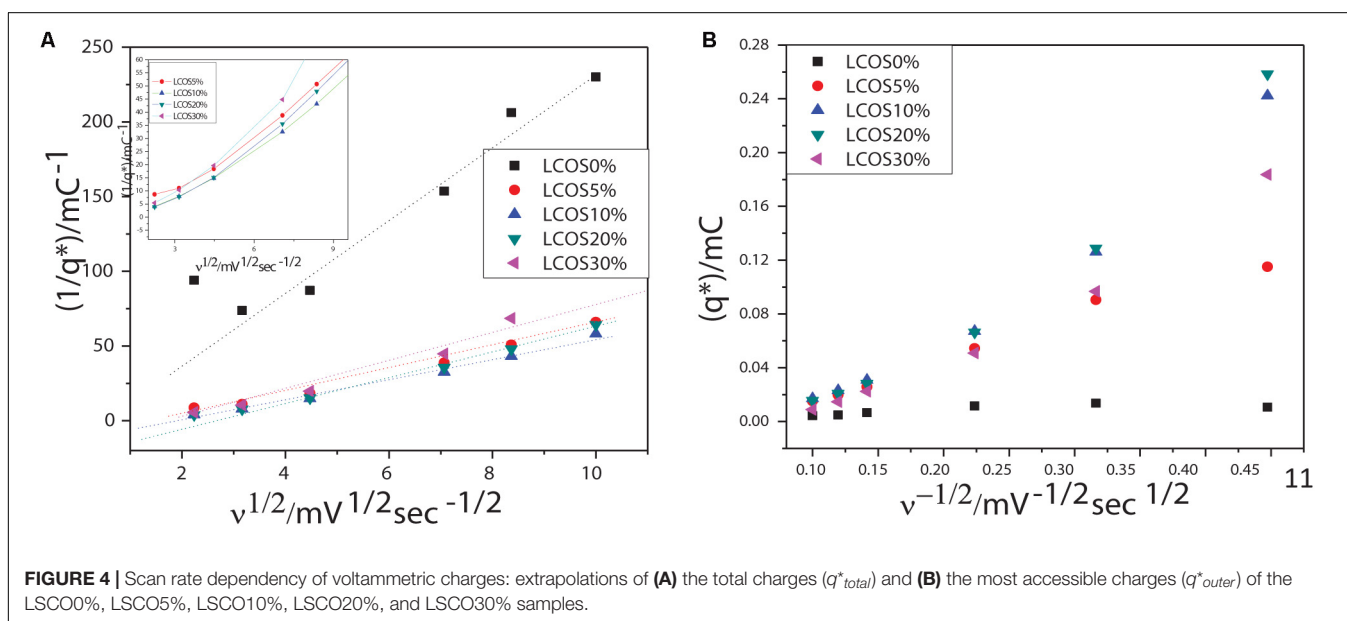
Generally, the number of catalyst active sites or active surface areas are considered proportional to voltammetry charges q^*

(Ardizzone et al., 1990; Wu et al., 2011). Calculation of q^* is determined following Eq. 2 as reported by Audichon et al. (2014), Mohan and Mao (2018), Mao et al. (2019).

$$q^* = \frac{1}{\gamma_{ms}} \int_{E_1}^{E_2} i(E) dE \quad (2)$$

Briefly, q^* value is the average of anodic and cathodic charges measured between 0.4 and 1 V vs RHE. The calculated q^* values for the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples are summarized in **Table 2**.

Ardizzone and co-workers established two relations as following Eqs 3 and 4 which depend on the basis of diffusion species phenomena at the interface of the electrode/electrolyte depending on the scan rate (Ardizzone et al., 1990).

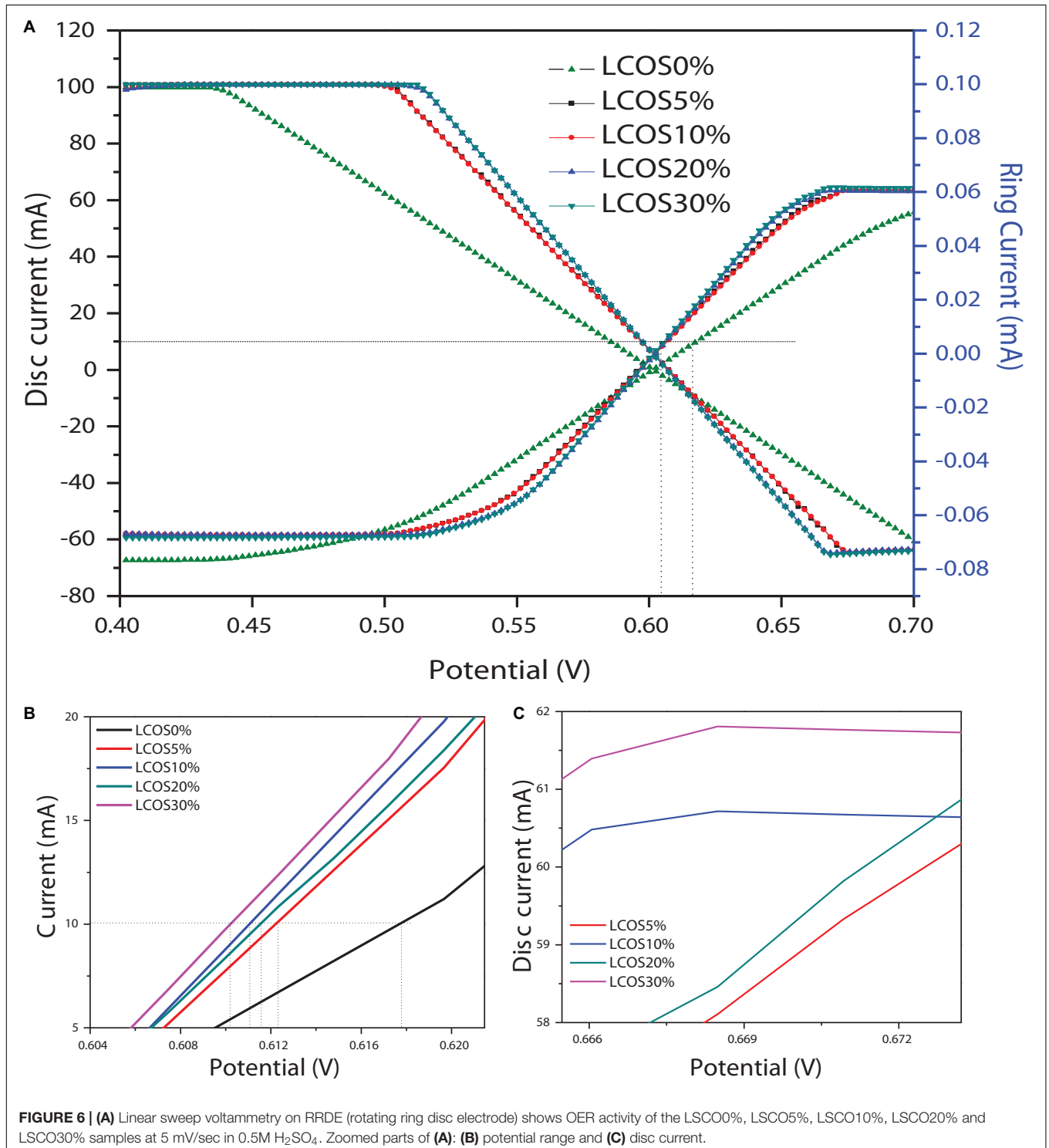


Following Eqs 3 and 4, the total charges (q^*_{total}) and the most accessible charges (q^*_{outer}) were determined when the scan rate values tend to 0 and ∞ , respectively (Cheng et al., 2009).

$$q^* = q^*_{outer} + C_1 \frac{1}{\sqrt{\nu}} \quad (3)$$

$$\frac{1}{q^*} = \frac{1}{q^*_{total}} + C_2 \sqrt{\nu} \quad (4)$$

where C_1 and C_2 are constants, ν is the scan rate, and q^* are the average charges calculated for different scan rates included between 5 to 100 mV/s. The q^*_{total} and q^*_{outer} values



for crystalline oxides samples are obtained by linear part extrapolations of the curves presented in **Figure 4** and are summarized in **Table 3**.

The calculated total charges q^*_{total} of the LSCO30% (0.765 mC) and LSCO20% (1.416 mC) samples synthesized by the combined sol-gel and molten-salt process are the lowest compared with the LSCO0% (33.6 mC), LSCO5% (5.47 mC), and LSCO10% (4.68 mC) samples. The supposition established from the capacitance measurements therefore confirms that the number of active sites increases and promotes the charge accumulation properties of the catalyst when the mean crystallite size decreases. The highest value for the most accessible charge q^*_{outer} was obtained for the LSCO20% sample (0.0206 mC), followed by the LSCO10% (0.0156 mC), LSCO30% (0.009 mC), LSCO5% (0.005 mC) samples, and then the LSCO0% sample (0.0026 mC). The synthesized LSCO20% sample has allowed one to obtain a higher number of accessible active sites in the catalytic layer, which is probably due to the higher concentration of active sites on the surface and the stability of the catalyst at the electrode surface. Moreover, from the obtained charge values, the active site's accessibility was evaluated by the ratio q^*_{outer}/q^*_{total} (**Table 2**). The highest active site's accessibility was obtained from the LSCO20% sample (0.0145) and followed by the LSCO30% (0.0128), LSCO10% (0.0033), and LSCO5% (0.00104) samples, whereas the one with the lowest q^*_{outer}/q^*_{total} ratio was measured from the LSCO0% sample (0.000078).

Stability Test

Repetitive CV measurement was achieved to assess these oxide samples' electrochemical activity and stability (Cheng et al., 2009). As shown in **Figure 3**, 100 voltammetric cycles were carried out between 0.4 and 1 V vs RHE in 0.5 mol l⁻¹ H₂SO₄ at 20 mV s⁻¹ with the aim of evaluating these catalysts' aging during a long-term test through their current density evolution.

For the five LSCO catalyst samples (**Figure 3**) no modification of the CV shapes appears during the long term 100 cycle test. This observation indicates that no alteration of the particles' structure, which composed the catalytic layer, occurs during the test. However, the current densities decrease during the first cycles and finally tend to stabilize. The fact that the cathodic and anodic current densities do not evolve drastically and no extra peaks appear reveals a high stability of the obtained LSCO oxide samples after heat treatment under variable transient conditions. The corresponding CVs of the synthesized LSCO samples overlap between the 5th and 10th cycles (**Figure 5**). The evolution of the current during the test could arise from a slight loss of active sites in the catalytic layer, which could contribute to a small catalytic performance decrease.

For different cycles of this stability test, the charge values (q^*) were measured to quantify the active-sites losses and the degradation of the electrocatalytic performances (**Figure 5**). According to the agreement with the CV observations, the calculated charges decrease in the first activation time (first 5–10 cycles). For the LSCO30%, LSCO20% and LSCO10% samples, the decrease takes place until the 10th cycle whereas for the LSCO5% and LSCO0% catalysts, it is less significant and occurs only for the first five cycles.

As the charges are considered to be proportional to the number of active sites, the $q^*/q^*_{initial}$ ratio as a function of the number of cycles may be used to evaluate the active site losses (**Figure 5**). The remaining active sites after 50 cycles for the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples are 84, 93, 92, 86, and 92% of the initial charges, respectively. As the CV shapes remain the same along the durability test, the charge ratio evolution could be attributed to the degradation of the catalytic layers, due to a slight erosion of the catalyst at the interface with the electrolyte (Da Silva et al., 1997).

Catalyst Used for OER Measurement

The OER activity of the LSCO samples was evaluated primarily by rotating ring disk electrode voltammetry (RRDE) at a 0.05 mV/s scan rate and 1600 rpm rotation rate. This scan rate is slow enough for steady-state behavior at the electrode surface, and the rotation rate is sufficiently fast to aid in product removal and limit bubble formation from evolved O₂ at the electrode surface. As shown in **Figure 6A**, the horizontal dashed line at 10 mA cm⁻² per geometric area is a significant figure of merit for the electroactive catalyst (Weber and Dignam, 1984; Matsumoto and Sato, 1986; Gorlin and Jaramillo, 2010; Walter et al., 2010). To evaluate the electrocatalytic properties of the oxide materials toward the OER as well as their behavior during this reaction, linear sweep voltammetry measurements were performed. For our LSCO samples (**Figure 6A**), current was first normalized to the geometric surface area of the working electrode to compare the catalytic performance of the LSCO samples as the same masses were deposited on the electrode. It demonstrated that the LSCO20% and LSCO30% samples have better electrocatalytic efficiency for OER than the LSCO0%, LSCO5%, and LSCO10% samples. Specifically, the obtained current densities of the LSCO0%, LSCO5%, LSCO 10%, LSCO20%, and LSCO30% samples are 55.28, 60.29, 60.6, 60.8, and 61.7 mA, respectively. The zoom parts of overpotential (**Figure 6B**) and disk current (**Figure 6C**) give a clearer demonstration of the trend.

Electrochemically Active Surface Area

The electrochemically active surface area (ECSA) of the LSCO samples was estimated from the electrochemical double-layer capacitance of the catalytic surface (Trasatti and Petrii, 1991). The electrochemical capacitance was determined by measuring the non-Faradaic capacitive current associated with double-layer charging from the scan-rate dependence of CVs shown in **Figure 3** (Trasatti and Petrii, 1991; Benck et al., 2012;

TABLE 4 | Comparison between ECSA and RF values of the LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples.

Catalyst	ECSA (cm ²)	RF
LSCO0%	0.4538	0.0903
LSCO5%	0.0426	0.0849
LSCO10%	0.0717	0.1428
LSCO20%	0.0903	0.1799
LSCO30%	0.0791	0.1576

Ouyang et al., 2019; Wang et al., 2020). Ideal catalysts for OER should have low overpotentials, be stable over time, and have high specific activity (or low surface area) (Mahmood et al., 2013). Electrochemically active surface area was calculated based on $ECSA = C_{dl}/C_s$ where C_{dl} and C_s are double layer capacitance and specific capacitance, respectively.

The roughness factor (RF) is calculated by dividing the estimated ECSA by the geometric area of the electrode, 0.5024 cm². **Table 4** shows the obtained ECSA and roughness factor values for all five LSCO catalyst samples. Electrochemically active surface area value of the LSCO20% sample is 0.0903 cm², which is higher than the LSCO10% (0.0717 cm²), LSCO30% (0.791 cm²), LSCO5% (0.0426 cm²), and LSCO0% (0.4538 cm²) samples. Roughness factor values of the LSCO0% (0.0903) and LSCO5% (0.0849) are lower than the LSCO10% (0.1428), LSCO20% (0.1799), and LSCO30% (0.1576) samples.

CONCLUSION

In this paper, we report a combined sol-gel and molten salt synthesis (MSS) procedure to synthesize LSCO0%, LSCO5%, LSCO10%, LSCO20%, and LSCO30% samples. Moreover, we have demonstrated the electrocatalytic comparisons between the LSCO samples as electrode materials in terms of specific

capacitance, total charge, and charge accessibility. Cyclic voltammetry and a LSV on rotation ring disk electrode measurements show the enhanced electrocatalytic activity of LSCO. The resulting current density could be a function of both the surface area and the morphology of the LSCO samples used and a combination of both faradaic and non-faradaic procedure.

DATA AVAILABILITY STATEMENT

All datasets generated for this study are included in the article/supplementary material.

AUTHOR CONTRIBUTIONS

SM conducted the experiments. YM initiated the ideas and led the effort. Both authors contributed to the article and approved the submitted version.

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Conflict of Interest: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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