

Equation of state for CO and CO₂ fluids and its application on decarbonation reactions at high pressure and temperature

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1 **Abstract**

2 *Ab initio* molecular dynamics simulations were performed at pressures and temperatures up to
3 160 GPa and 4000 K, in order to obtain equations of state (EOS) for CO and CO₂ fluids. We found
4 that polymerisation of CO and CO₂ fluids starts at low pressures, and that including the effect of
5 polymerisation is essential for accurate EOS. EOSs for CO and CO₂ determined from methods
6 using experimental data, or classical potentials that ignore the changes in speciation, should be
7 treated with caution when extrapolated beyond the examined pressures and temperatures. The
8 obtained data was fitted into a modified Lee and Kesler EOS for both CO and CO₂ fluids. The
9 thermodynamic calculations for the decarbonation reactions of both MgCO₃ and CaCO₃ using the
10 derived CO₂ EOS reproduced the experimental data and theoretical calculations at low pressures.
11 Both MgCO₃ and CaCO₃ pure phases are found to be stable in the upper mantle compared to CO₂.
12 However, they both become destabilised when approaching lower mantle conditions.

13 **Keywords**

14 Decarbonation reaction; equation of state; CO₂ fluid; CO fluid; polymerisation; carbonate

15 **1 Introduction**

16 Accurate descriptions of P-V-T (Pressure-Volume-Temperature) data and thermal properties of
17 CO and CO₂ fluids are needed for a complete and robust thermophysical description of the Earth's
18 mantle. Such knowledge is also important for understanding the interiors of giant planets such as
19 Neptune, Uranus and the many similar exoplanets that are composed of C, H, O and N under high
20 pressures and temperatures (Cavazzoni et al., 1999; Hubbard, 1981). Furthermore, the fundamental
21 questions on the evolution of molecular bonding with increasing pressure and temperature also
22 prompt the study of CO and CO₂ at high P/T conditions (Bernard et al., 1998; Datchi et al., 2009;
23 Iota et al., 2006; Santoro and Gorelli, 2006). The study of molecular fluids like CO and CO₂ under
24 extreme conditions can not only help to understand their basic chemistry, but also is of general
25 interest in materials science, geoscience and industry.

26 Significant effort has been devoted to the determination of the equations of state (EOS) and the
27 properties of CO and CO₂ fluids under the conditions of planetary interiors. However, there are
28 relatively few experimental data on CO and CO₂ fluids at high P/T conditions, with most studies
29 at high P & T being theoretical. Belonoshko and Saxena used classical molecular dynamics (MD)

30 with a Buckingham potential to determine the EOS of volatile fluids (Belonoshko and Saxena,
31 1991a; Belonoshko and Saxena, 1992). They calculated the EOS of CO₂ fluid (BS-1992 EOS) in
32 the range from 400 to 4000 K and from 0.5 to 100 GPa (Belonoshko and Saxena, 1992). Churakov
33 and Gottschalk extended the EOS of CO₂ fluid (CG-2003 EOS) to 10000 K based on
34 thermodynamic perturbation theory (Churakov and Gottschalk, 2003). Duan and Zhang obtained
35 an EOS for CO₂ fluid (DZ-2006 EOS) based on *ab initio* calculations and experimental data from
36 0 GPa to 10 GPa and from 673 K to 2573 K (Duan and Zhang, 2006). Recently, Fu et al. (2017)
37 formulated an EOS (FB-2017 EOS) based on several hundred *ab initio* molecular dynamics
38 (AIMD) calculations performed between 0.5 and 104 GPa and from 600 to 4000 K for CO₂; they
39 found substantial differences in EOS with some of the empirical potential results of Churakov and
40 Gottschalk (2003) and Belonoshko and Saxena (1992). In the case of CO fluid, Belonoshko and
41 Saxena derived an EOS of CO fluid (BS-1991 EOS), again using classical MD (Belonoshko and
42 Saxena, 1991b). More recently, Leonhardi performed AIMD simulations to characterise CO fluid
43 to 140 GPa and 5000 K and obtained an EOS (Leonhardi-2017 EOS; (Leonhardi and Militzer,
44 2017). Several shock-wave experiments exist on CO and CO₂, potentially allowing an assessment
45 of the various EOSs, however little accurate temperature determination exists (Nellis et al., 1991;
46 Nellis et al., 1981). Notably, in the shock experiments, CO and CO₂ molecules decomposed at
47 high P and condensed into the diamond phase.

48 In this study, we perform AIMD simulations to determine the structural evolution and EOSs of
49 CO and CO₂ fluids at temperatures from 1000 to 4000 K and pressures from 0 to 160 GPa. We
50 find that pressure has little effect on the intramolecular C-O bond length in both CO and CO₂. Both
51 CO and CO₂ fluids exhibit increased polymerisation from low pressures to high pressures, which
52 is due to the pressure-induced intermolecular bonding. We show convincingly that polymerisation
53 is a pressure driven process. The change of speciation of CO and CO₂ fluids by polymerisation
54 suggests results in the literature based on classical methods or extrapolation from experimental
55 data need to be re-evaluated. We apply the derived EOS to decarbonation reactions of MgCO₃ and
56 CaCO₃, and obtain results which agree well with experimental data at low pressures.

57 **2 Methods**

58 2.1 AIMD simulations at high P/T conditions

59 We performed Born–Oppenheimer AIMD calculations based on density functional theory
60 (DFT). We used the VASP code (Blöchl, 1994; Kresse and Joubert, 1999), PAW potentials (Kresse
61 and Furthmüller, 1996; Kresse and Hafner, 1993) (with valence configurations $2s^22p^2$ and $2s^22p^4$
62 for C and O, respectively) and a planewave cut-off of 500 eV. We used a supercell containing 64
63 molecules for both CO₂ and CO. The Brillouin zone was sampled with the Γ -point. This setting
64 converged the pressure to within 0.2 GPa. Exchange-correlation effects were treated in the
65 generalized gradient approximation (GGA) with the Perdew-Burke-Ernzerhof (PBE) (Perdew et
66 al., 1996) scheme. Single particle orbitals were populated according to the Fermi–Dirac statistics.
67 The integration (with the time step of 1.0 fs) of the classical Newton’s equations of motion uses
68 the Verlet algorithm, and the ground-state search is done within an efficient iterative matrix
69 diagonalization scheme and a Pulay mixer for each step. We ran NVT simulations at the target
70 temperatures and pressures; the temperature was controlled by a Nosé thermostat (Di Tolla and
71 Ronchetti, 1993; Nosé, 1984); these simulations were run for over 5 ps and up to 30 ps depending
72 on the equilibration time. Stresses were averaged from NVT calculations within the production
73 period of at least 3 ps. The input structures were carefully prepared using the Packmol code
74 (Martínez et al., 2009), in which the intermolecular distances (>1.6 Å) are larger than the
75 intramolecular bond lengths.

76 2.2 EOS for CO and CO₂ fluids

77 For CO and CO₂ fluids, the calculated P-V-T data were fitted into the Lee and Kesler equation
78 (Lee Byung and Kesler Michael, 1975) modified by Duan and Zhang (2006)

$$79 \quad \frac{PV}{RT} = \mathbf{1} + \frac{B}{v_r} + \frac{C}{v_r^2} + \frac{D}{v_r^4} + \frac{E}{v_r^5} + \frac{F}{v_r^2} \left(\beta + \frac{\gamma}{v_r^2} \right) \exp \left(-\frac{\gamma}{v_r^2} \right) \quad (1)$$

80 where

$$81 \quad v_r = \frac{v}{v_c} \quad (2)$$

$$82 \quad B = a_1 + \frac{a_2}{T_r^2} + \frac{a_3}{T_r^3} \quad (3)$$

$$83 \quad C = a_4 + \frac{a_5}{T_r^2} + \frac{a_6}{T_r^3} \quad (4)$$

$$84 \quad D = a_7 + \frac{a_8}{T_r^2} + \frac{a_9}{T_r^3} \quad (5)$$

$$85 \quad E = a_{10} + \frac{a_{11}}{T_r^2} + \frac{a_{12}}{T_r^3} \quad (6)$$

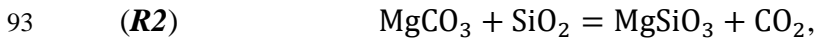
86
$$F = \frac{\alpha}{T_r^3} \quad (7)$$

87
$$T_r = \frac{T}{T_c} \quad (8)$$

88 R is the gas constant; T is the temperature and V is the volume; V_C and T_C are the critical volume
 89 and temperature, respectively; a_1 to a_{12} , α , β and γ are fitting parameters.

90 2.3 Thermodynamic calculation of decarbonation reactions

91 We applied the derived EOS of CO₂ fluid to the following decarbonation reactions:



96 The Gibbs free energy of formation from the elements at a pressure and temperature is given
 97 by

98
$$G_{p,T} = G_{f(1 \text{ bar}, T)}^\circ + \int_{1 \text{ bar}}^p V_T(p) dp$$

99
$$= H_{f(1 \text{ bar}, 298 \text{ K})}^\circ - T S_{f(1 \text{ bar}, 298 \text{ K})}^\circ + \int_{1 \text{ bar}, 298 \text{ K}}^T C_{p(1 \text{ bar})}(T) dT - T \int_{1 \text{ bar}, 298 \text{ K}}^T C_{p(1 \text{ bar})}(T)/T dT +$$

100
$$\int_{1 \text{ bar}, T}^P V_T(p) dp \quad (9)$$

101 where $G_{f(1 \text{ bar}, T)}^\circ$ is the Gibbs free energy of formation at 1 bar and T , $H_{f(1 \text{ bar}, 298 \text{ K})}^\circ$ and $S_{f(1 \text{ bar}, 298 \text{ K})}^\circ$
 102 are the standard enthalpy and entropy of formation, respectively; $C_{p(1 \text{ bar})}$ is the isobaric specific
 103 heat capacity at 1 bar and $V_T(p)$ is the volume at p under constant T .

104 By using the EOS of CO₂ fluid obtained above, the Gibbs free energy at specific P & T can be
 105 calculated with the available experimental $G_{f(1 \text{ bar}, T)}^\circ$. For the minerals involved in the
 106 decarbonation reactions, we used existing EOS from the literature, except for magnetite where we
 107 refitted the PVT data to encompass a volume dependent Anderson-Grüneisen parameter δ_T . In
 108 Table S1, we list the thermodynamic quantities taken from literature.

109 Specifically, we used a high temperature Birch-Murnaghan (HTBM) EOS for both MgCO₃ and
 110 MgO, following (Redfern et al., 1993). The third-order BM EOS is given by

$$P(V) = \frac{3B_0}{2} \left[\left(\frac{V_0}{V} \right)^{7/3} - \left(\frac{V_0}{V} \right)^{5/3} \right] \left\{ 1 + \frac{3}{4} (B'_0 - 4) \left[\left(\frac{V_0}{V} \right)^{2/3} - 1 \right] \right\} \quad (10)$$

where B_0 , V_0 and B'_0 are the isothermal bulk modulus, equilibrium volume and pressure derivative of B_0 to pressure at ambient conditions, respectively. The temperature dependence of volume is described by using the volume-dependent Anderson-Gruneisen parameter δ_T

$$\delta_T = - \left(\frac{1}{\alpha B_T} \right) \left(\frac{\partial B_T}{\partial T} \right)_p = \left(\frac{\partial \ln(\alpha)}{\partial \ln(V)} \right)_T = \frac{V}{V_0} \cdot m - 1 \quad (11)$$

where α is the volumetric thermal expansion coefficient, and m is a dimensionless parameter (Chopelas and Boehler, 1992).

For MgSiO_3 , SiO_2 , CaCO_3 (*aragonite*, *arag*), CaO and CaSiO_3 , we used the form of HTBM used by Dubrovinsky and Swamy (1997); Litasov et al. (2008); Litasov et al. (2017); Oda et al. (1992); Swamy et al. (1994); Tange et al. (2012). In this form, B_0 , V_0 and B'_0 all become temperature dependent. The temperature dependence of the equilibrium volume is expressed by α

$$V_{1 \text{ bar}, T} = V_{1 \text{ bar}, 298.15 \text{ K}} \exp \left(\int_{298.15 \text{ K}}^T \alpha dT \right) \quad (12)$$

and the temperature dependence for B_0 and B'_0 is defined by $(\partial B_0 / \partial T)_p$ and $(\partial B'_0 / \partial T)_p$, respectively.

For other phases of CaCO_3 , we used the data produced by *ab initio* calculations from Zhang et al. (2018). The second form of HTBM was used to describe the EOSs under 900 K, and a Mie-Gruneisen EOS was used for temperatures over 900 K, according to Zhang et al. (2018). Details can be found in the original publication.

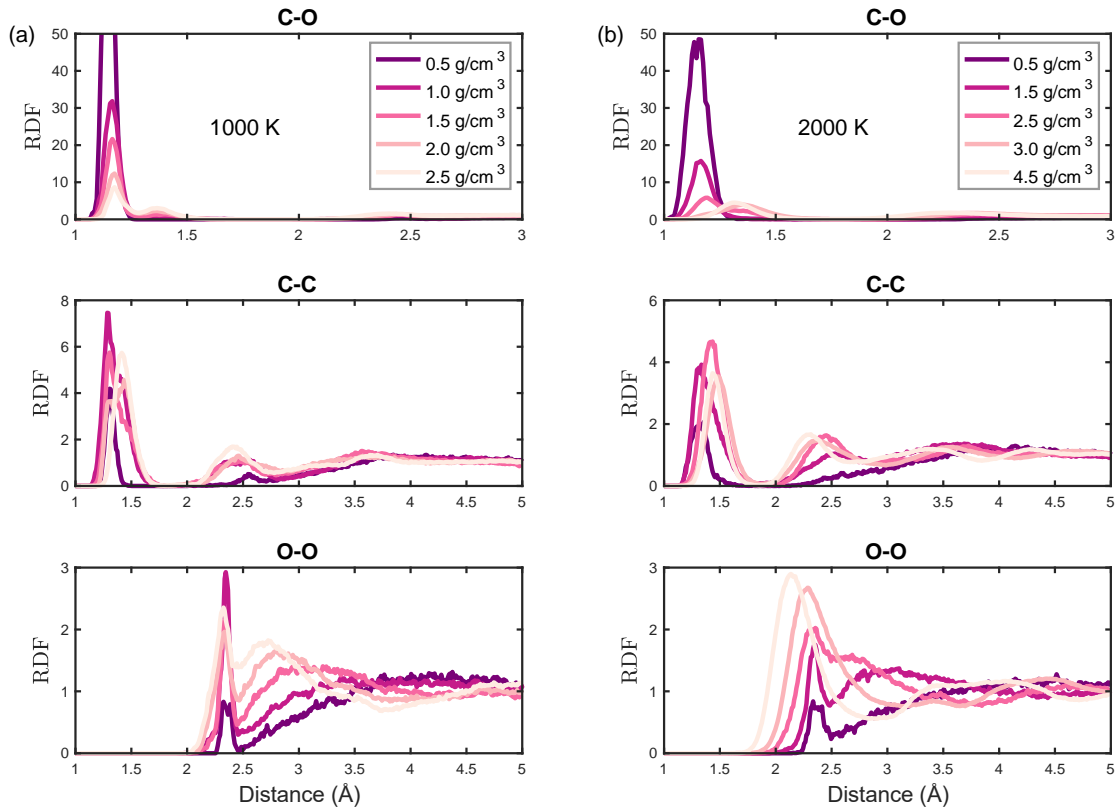
3 Results

3.1 Structure and polymerisation of CO and CO₂ fluids at high P/T conditions

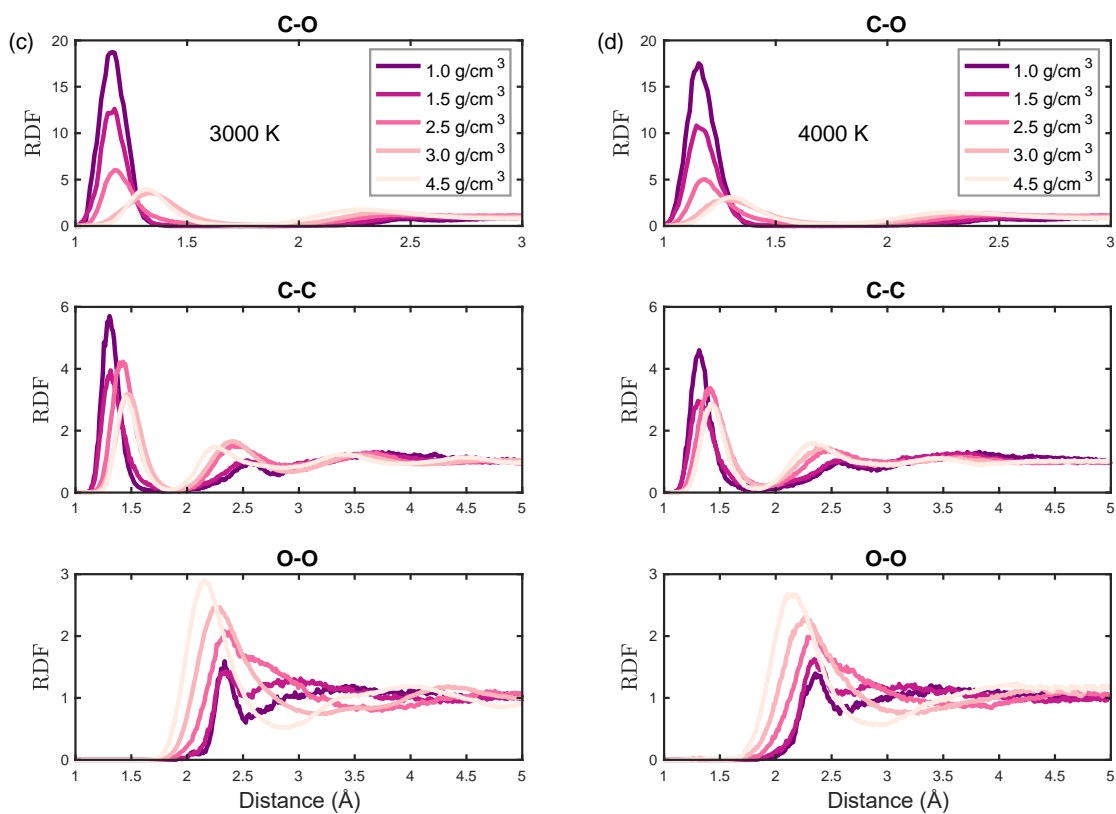
AIMD simulations were performed at temperatures of 1000, 2000, 3000 and 4000 K for both CO and CO₂, and at densities of 0.5 to 4.5 g/cm^3 . We expect from these simulations that not only the speciation of CO and CO₂ at high P/T conditions can be obtained, but also, we can better understand the evolution of molecular bonding with increasing pressure and temperature.

We analysed MD trajectories to obtain the structural information and extract the speciation information. We calculated the radial distribution function (RDF) for each atom in the system. The calculated RDFs for CO and CO₂ fluids are shown in Figures 1 and 2 (and in Supplementary

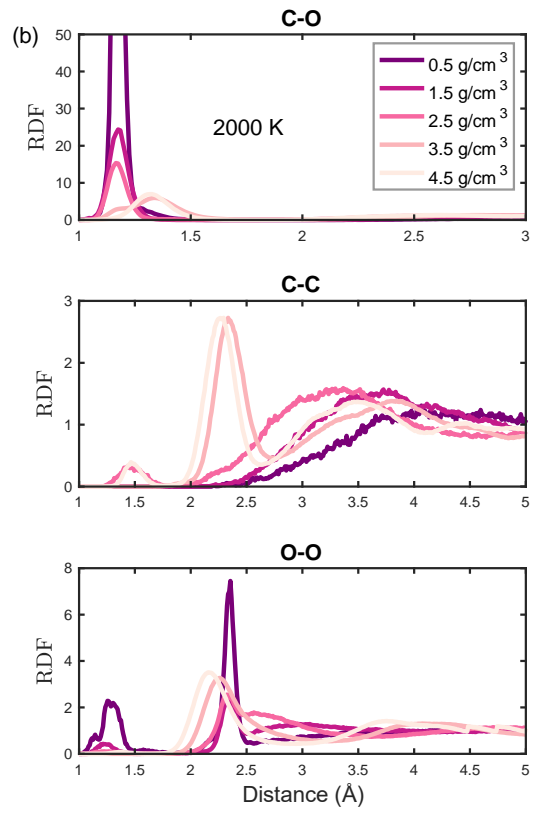
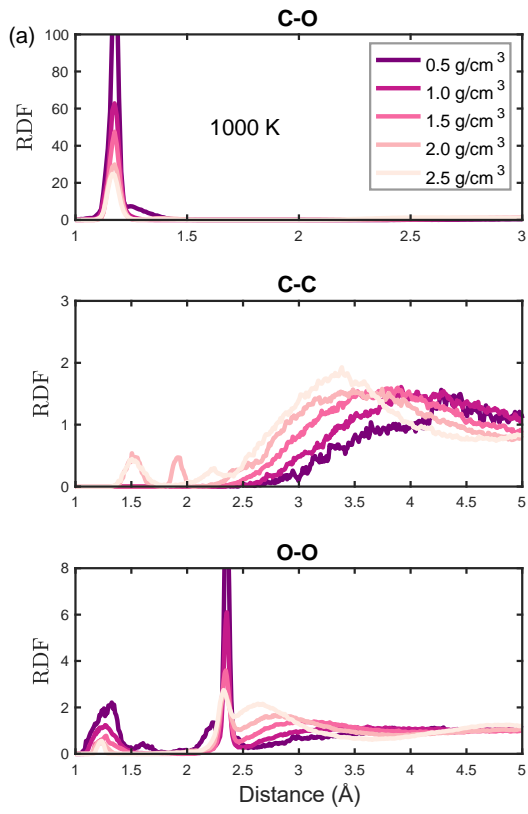
138 Materials (SM)), and the speciation of CO and CO₂ fluids is shown in Table 1. We collected the
139 average pressure for each run and the results are also shown in Table 1.

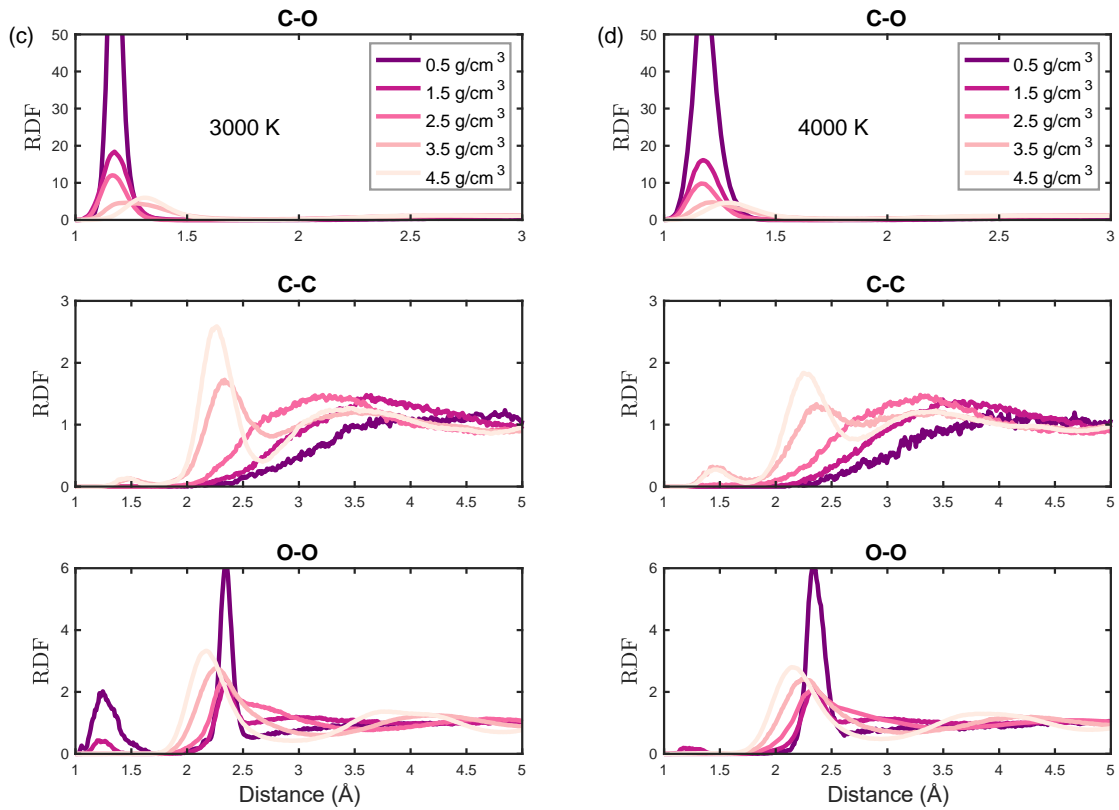


140



141
 142 **Figure 1.** Calculated radial distribution functions (RDFs) in CO fluid at 1000, 2000, 3000 and
 143 4000 K under different densities (pressures). The main C-O peak at *ca.* 1.17 Å belongs to CO and
 144 CO₂ molecules. The C-C peaks at *ca.* 1.37 Å and 2.48 Å indicate the polymerisation of CO fluid.





146
 147 **Figure 2.** Radial distribution functions in CO₂ fluid at 1000, 2000, 3000 and 4000 K under
 148 different densities (pressures). The main C-O peak at *ca.* 1.17 Å belongs to CO and CO₂
 149 molecules. The C-C peaks at *ca.* 1.41 Å and 2.48 Å indicate the polymerisation of CO fluid. The
 150 O-O peak at *ca.* 1.25 Å corresponds to the bond length in the O₂ molecule.

151 **Table 1.** Calculated P-V-T data and the population of different species. The calculation of
 152 molecular CO, CO₂ and polymerised C populations is based on the total C budget of the system,
 153 and the calculation of molecular O₂ population is based on the O budget of the system.

Fluid	Temperature (K)	Pressure (GPa)	Volume (cm ³ /mol)	Density (g/cm ³)	Population (%)			
					CO	CO ₂	O ₂	Polymerised C
CO	1000 K	0.27	56.02	0.5	89.06	3.13	0.00	7.81
	1000 K	1.00	28.01	1.0	38.91	16.72	0.00	44.38
	1000 K	3.86	18.67	1.5	24.22	15.31	0.00	60.47
	1000 K	8.20	14.00	2.0	8.59	11.72	0.00	79.69
	1000 K	15.25	11.20	2.5	2.03	10.78	0.00	87.19
	2000 K	0.48	56.02	0.5	83.59	2.97	0.00	13.44
	2000 K	1.93	28.01	1.0	37.81	16.09	0.00	46.09
	2000 K	5.88	18.67	1.5	23.13	13.13	0.00	63.75
	2000 K	10.54	14.00	2.0	7.81	13.28	0.00	78.91
	2000 K	18.16	11.20	2.5	0.16	6.25	0.00	93.59

	2000 K	29.58	9.34	3.0	0.00	0.00	0.00	100
	2000 K	49.39	8.00	3.5	0.00	0.00	0.00	100
	2000 K	147.64	6.22	4.5	0.00	0.00	0.00	100
	3000 K	2.56	28.01	1.0	37.66	12.97	0.00	49.38
	3000 K	7.62	18.67	1.5	20.47	12.34	0.00	67.19
	3000 K	12.55	14.00	2.0	3.44	13.59	0.00	82.97
	3000 K	23.26	11.20	2.5	0.31	6.56	0.00	93.13
	3000 K	37.65	9.34	3.0	0.00	2.50	0.00	97.50
	3000 K	55.07	8.00	3.5	0.00	0.00	0.00	100
	3000 K	149.61	6.22	4.5	0.00	0.00	0.00	100
	4000 K	3.27	28.01	1.0	34.84	11.41	0.00	53.75
	4000 K	8.33	18.67	1.5	17.03	10.16	0.00	72.81
	4000 K	25.82	11.20	2.5	0.63	4.53	0.00	94.84
	4000 K	42.04	9.34	3.0	0.00	0.78	0.00	99.22
	4000 K	67.39	8.00	3.5	0.00	0.00	0.00	100.00
	4000 K	160.53	6.22	4.5	0.00	0.00	0.00	100.00
	1000 K	0.10	88.02	0.5	30.00	64.38	3.67	5.63
	1000 K	0.91	44.01	1.0	27.66	70.78	9.92	1.56
	1000 K	3.75	29.34	1.5	16.09	79.69	2.11	4.22
	1000 K	9.58	22.00	2.0	11.56	72.97	2.27	15.47
	1000 K	22.21	17.60	2.5	1.82	64.12	9.38	34.06
	1000 K	49.19	12.57	3.5	0.00	3.20	69.16	96.80
	2000 K	0.38	88.02	0.5	24.83	72.58	5.79	2.60
	2000 K	1.44	44.01	1.0	26.10	70.26	3.86	3.64
	2000 K	4.53	29.34	1.5	15.31	78.91	3.05	5.78
	2000 K	12.56	22.00	2.0	3.82	80.80	2.25	15.35
	2000 K	25.62	17.60	2.5	1.88	64.06	1.56	34.06
	2000 K	39.63	14.67	3.0	0.00	2.74	2.16	97.26
	2000 K	50.67	12.57	3.5	0.00	1.66	0.00	98.34
	2000 K	85.68	11.00	4.0	0.00	0.00	8.13	100
	2000 K	132.94	9.78	4.5	0.00	0.00	0.00	100
	3000 K	0.64	88.02	0.5	24.53	75.47	2.16	0.00
	3000 K	2.24	44.01	1.0	25.69	62.36	5.95	11.95
	3000 K	5.95	29.34	1.5	12.81	64.84	3.28	22.34
	3000 K	14.31	22.00	2.0	3.75	53.91	1.95	42.34
	3000 K	29.02	17.60	2.5	1.09	32.03	0.70	66.88
	3000 K	46.50	14.67	3.0	0.94	14.84	0.16	84.22
	3000 K	50.67	12.57	3.5	0.00	0.00	0.00	100

CO₂

3000 K	90.75	11.00	4.0	0.00	0.00	0.00	100
3000 K	132.94	9.78	4.5	0.00	0.00	0.00	100
4000 K	0.72	88.02	0.5	0.82	90.74	0.00	8.44
4000 K	6.86	29.34	1.5	10.16	72.03	2.11	17.81
4000 K	15.94	22.00	2.0	6.72	54.69	2.34	38.59
4000 K	30.83	17.60	2.5	1.56	39.22	0.39	59.22
4000 K	48.21	14.67	3.0	0.59	17.24	0.35	82.17
4000 K	71.08	12.57	3.5	0.31	4.69	0.16	95.00
4000 K	103.61	11.00	4.0	0.00	0.00	0.43	100
4000 K	151.80	9.78	4.5	0.00	0.00	0.00	100

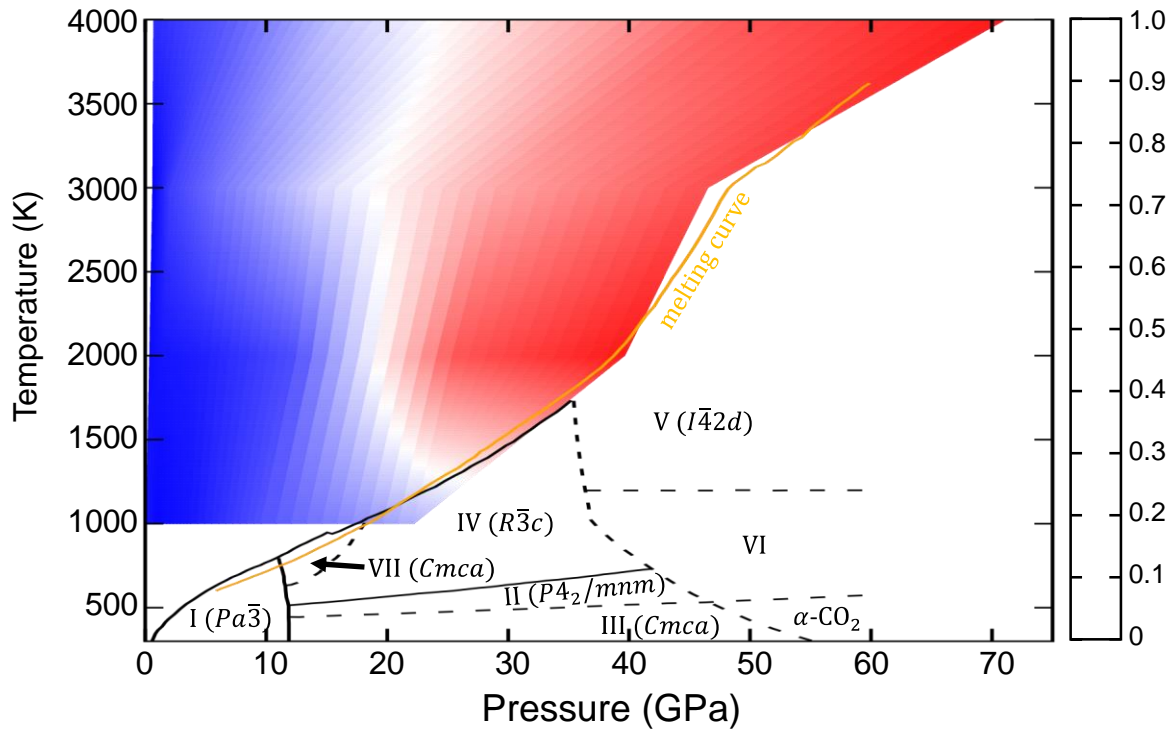
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155 The RDFs for CO fluid in Figure 1 clearly show that the main C-O peak at *ca.* 1.17 Å is
156 continuously weakened with the increasing density/pressure at all temperatures, but the position
157 of the peak remains almost the same. At the same time, a shoulder peak at *ca.* 1.36 Å starts to
158 appear. This arising peak corresponds to the C-O bond in the polymerised segments. The change
159 of C-O peaks suggests the continuous dissociation of CO molecules due to the establishment of
160 intermolecular bonding and the stability of C-O intramolecular bonding character with increasing
161 pressure. Also, in Figure 1, we can see the growth of a C-C peak at *ca.* 1.37 Å, which suggests the
162 direct bonding between C atoms of neighbouring CO molecules. Both the C-C peak at *ca.* 1.37 Å
163 and C-O peak at *ca.* 1.36 Å belong to the polymerised segments. With increasing pressure, a second
164 C-C peak at *ca.* 2.48 Å also becomes more and more prominent, and at about the same position an
165 O-O peak also becomes more evident. These two peaks correspond to the C-X-C (X denotes C or
166 O) and O-C-O bond lengths, respectively. There is no O-O peak at the O-O bond length (1.21 Å
167 in the gas state) of O₂ molecules. We calculated the population of different species at different P/T
168 conditions by averaging their occurrences over time, which is listed in Table 1. We can see that
169 the population of CO molecules decreased from 89.06% to 2.03% from 0.27 GPa to 15.25 GPa at
170 1000 K. CO₂ molecules immediately appeared even at 0.27 GPa, which accounts for only 3.13%
171 of the total C budget. The population of CO₂ molecules quickly increased to its peak value of
172 16.72% at 1.00 GPa and then decreased with increasing pressure. The situation at other
173 temperatures are similar to those at 1000 K. The population of polymerised C continuously
174 increased with the increasing pressure, which reached up to 100% at 67.39 GPa and 4000 K. The
175 solidified structure (see Figure S3 in **SM**) contains tetrahedrally coordinated C and O. Specifically,
176 it contains diamond-like motifs, CO₄ tetrahedra and the intermediate mixtures of these two units.

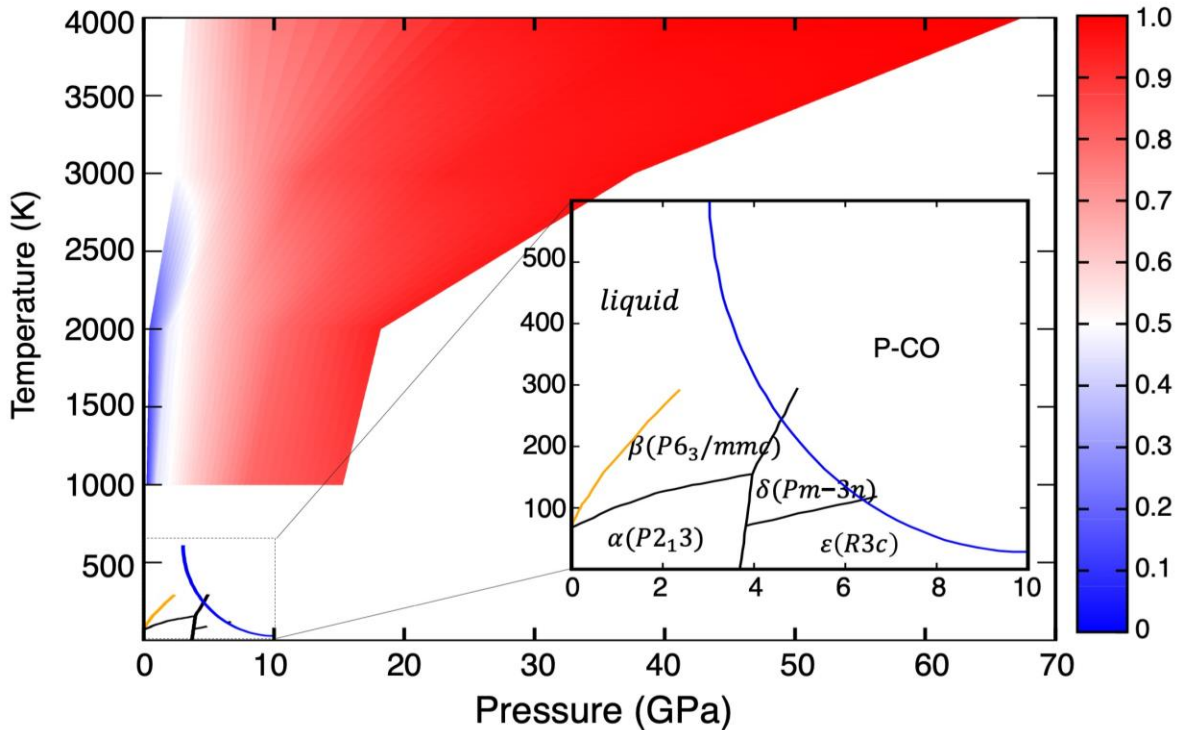
177 From the CO₂ phase diagram, we can see that the thermodynamically stable phase at the range of
178 35 to 60 GPa is a quartz-like CO₂-V that is composed of CO₄ tetrahedra. The solidified structure
179 of CO suggests that the stable phases could be diamond and CO₂-V when the fluids crystallise.

180 We perform a similar analysis on CO₂ fluid. As with CO fluid, the intensity of the main C-O
181 peak at *ca.* 1.17 Å continuously decreases with increasing pressure at all temperatures, while the
182 position of the peak remains almost the same, as can be seen in Figure 2. This reconfirms the
183 finding in CO fluid that the intermolecular bonding will be gradually established while the
184 intramolecular bonding remains the same under increasing pressure. In Figure 2, we can also see
185 a C-C peak at *ca.* 1.48 Å that corresponds to the C-C direct bonding and a second C-C peak at *ca.*
186 2.41 Å that corresponds to the C-X-C bond. Together with the O-O peak at *ca.* 2.29 Å, this suggests
187 the polymerisation of CO₂ fluid. One difference from the CO fluid is that there is an additional C-
188 C peak at *ca.* 1.93 Å at 1000 K and 2.0 g/cm³ (9.58 GPa). This peak corresponds to the C-C bond
189 length in a very special molecule C₃O₆ (coordinates listed in Table S2 in **SM**), unique to this P/T
190 condition and, as far as we are aware, not seen before in the literature. An O-O peak appears at *ca.*
191 1.25 Å at low pressures that belongs to O₂ molecules, which was not seen in CO fluids. From the
192 population of different species in CO₂ fluid listed in Table 1, we can see that the population of
193 CO₂ molecules generally drops with increasing pressure. There is a considerable concentration of
194 CO molecules at low pressures; the CO population is 30% at 0.10 GPa and 1000 K, but it decreases
195 with increasing pressure and drops to an insignificant amount at high pressures. O₂ molecules
196 existed in CO₂ fluid at all conditions but never in a significant amount. The population of
197 polymerised C continuously increased with the increasing pressure, and 92.19% CO₂ molecules
198 were polymerised at 71.08 GPa and 4000 K. However, the structure was not solidified, even with
199 92.19% polymerisation, and the fluid is mainly composed of -C-O-C- chains and CO₄ tetrahedra
200 (see Figure S3 in **SM**). Some molecules and -C-C-C- chains also exist.

201 We find a common phenomenon shared by both CO and CO₂ fluids that polymerisation
202 proceeds as a result of the establishment of intermolecular bonding and the intramolecular bonding
203 is hardly affected. The number of the original intramolecular bonds in CO and CO₂ molecules are
204 reduced with the polymerisation, but the bond lengths of the remaining intact CO and CO₂
205 molecules hardly change. We plot the population of polymerisation in the P-T phase diagram in
206 Figures 3 and 4, which show clearly that polymerisation is mainly dependent on pressure.



207
 208 **Figure 3.** P-T phase diagram of CO₂. The black and orange lines show phase boundaries from the literature (Giordano and Datchi, 2007; Giordano et al., 2006; Gorelli et al., 2004; Iota and
 209 Yoo, 2001; Litasov et al., 2011; Teweldeberhan et al., 2013). Solid lines indicate a
 210 thermodynamic phase transition and the dashed lines indicate a kinetic transition. The orange
 211 line indicates the melting curve determined from *ab initio* simulations (Teweldeberhan et al.,
 212 2013). Coloured region indicates the P-T domain explored in this study and the extent to which
 213 polymerisation occurs (0-100%, blue to red).
 214



215 **Figure 4.** P-T phase diagram of CO. The black and orange lines show the phase boundaries
 216 (Cromer et al., 1983; Fukushima et al., 1977; Serdyukov et al., 2010). The blue line indicates the
 217 boundary between polymerised CO and the solid phases. The orange line represents the
 218 solid/liquid boundary. Coloured region indicates the extent to which polymerisation occurs (0-
 219 100%, blue to red).
 220

221 3.2 EOS of CO and CO₂

222 As discussed above, the polymerisation of CO₂ can go up to 95% while still in the liquid.
 223 Although some simulations extend into the solid phase field, they are metastable liquids and so are
 224 not used to fit the EOS. For CO, there is no melting information available at high P & T and so
 225 we neglected the data with 100% polymerisation in the fitting of EOS. In addition, we included
 226 the low P & T EOS data for CO₂ (up to 0.8 GPa and 1100 K) from Span and Wagner (1996) and
 227 EOS data for CO (up to 0.1 GPa and 1000 K) from Goodwin (1985) in the fitting, as low-pressure
 228 data is important for the accuracy of Gibbs free energy calculation. The data was fitted into a
 229 modified Lee-Kesler EOS, and the derived parameters are shown in Table 2. The obtained CO₂
 230 EOS is valid from 298.15 to 4000 K and 1 bar to 70 GPa, and the CO EOS is valid from 298.15 to
 231 4000 K and 1 bar to 40 GPa.

232 **Table 2.** Derived parameters for the modified Lee-Kesler EOSs (see eqs. (1-8)) of CO and CO₂
 233 fluids. The uncertainty in pressure is less than 10% on average in the region studied.

Parameter	CO ₂	CO
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V_C (cm ³ /mol)	94.0	92.166
T_C (K)	304.1	132.85
a_1	-0.060417280674	0.039835176862
a_2	29.312930805997	-2.543808448869
a_3	-26.741784606481	14.322113574972
a_4	0.582336809237	0.229238078128
a_5	-22.996326249305	-1.546458778437
a_6	-5.656015266431	-20.423296489026
a_7	-0.001944185691	-0.004813112395
a_8	2.276867190172	0.522356542096
a_9	-0.691325562713	1.397315140656
a_{10}	-0.000523527797	0.000336467163
a_{11}	-0.174510207149	-0.021999704023
a_{12}	-0.568501377298	-0.289945554888
α	-0.004054826576	-0.003542754107
β	-5328.542315117454	-3039.82823322819
γ	-0.047819433473	0.009093668377

234 4 Discussion

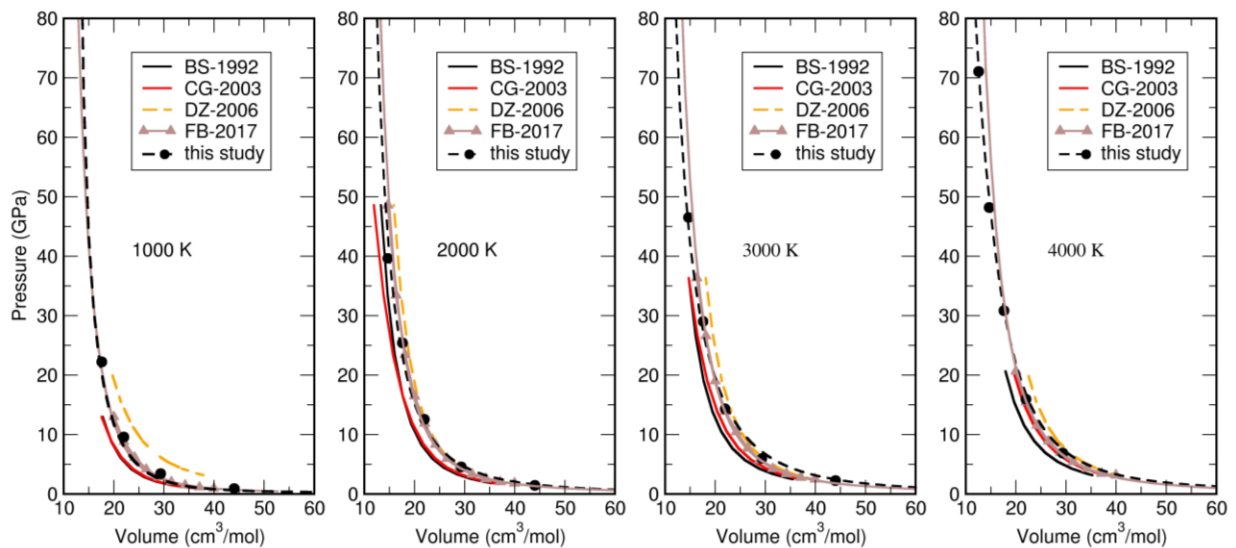
235 4.1 Comparison with previous EOS of CO and CO₂

236 Our EOS for CO₂ is compared in Figure 5 to those available in the literature, namely, BS-1992
237 (Belonoshko and Saxena, 1992), CG-2003 (Churakov and Gottschalk, 2003), DZ-2006 (Duan and
238 Zhang, 2006), and FB-2017 (Fu et al., 2017). BS-1992 and CG-2003 are very similar, but they lie
239 at lower pressures than both our results and FB-2017 for the same volumes. These two sets (BS-
240 1992 and CG-2003) are based on a classical potential fitted to experimental data at low pressures.
241 In contrast, DZ-2006 predicts the highest pressure among the five sets of EOS at the same volume.
242 DZ-2006 was also obtained by MD based on molecular potentials determined under room
243 temperature and pressure, and it was said to be valid in the temperature–pressure range from
244 673.15 to 2573.15 K up to 10.0 GPa. The final set discussed, FB-2017, was produced completely
245 from AIMD simulations. Their calculated results are in good agreement with our results.

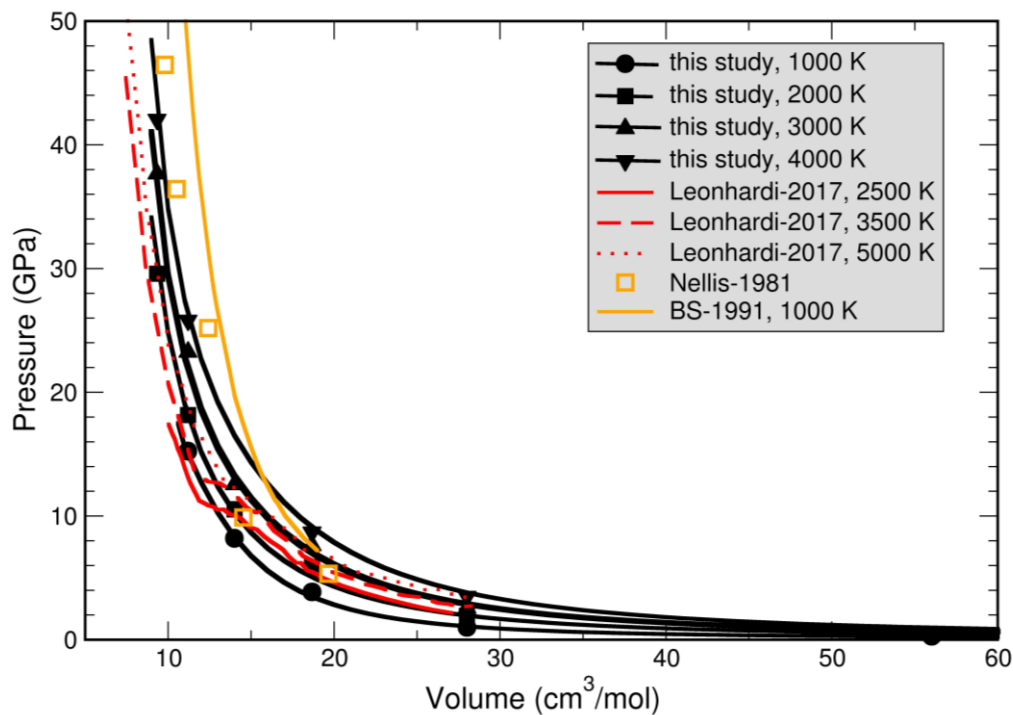
246 For CO fluids, we found one set of EOS data from classical MD simulations (BS-1991)
247 (Belonoshko and Saxena, 1991b), and one set of EOS data based on AIMD simulations
248 (Leonhardi-2017) (Leonhardi and Militzer, 2017). We plot them in Figure 6 together with our
249 results and the shock-wave data from Nellis et al. (1981). It was shown by Nellis’s experiment
250 (Nellis et al., 1981) that the CO fluids with molar volume less than 13 cm³/mol are all deeply
251 polymerised or solidified. Nellis also suggested a dense solid carbon phase at these conditions.
252 Our simulations also show a deeply polymerised CO with molar volume less than 13 cm³/mol. So,
253 our results agree with experiments in this regard. On the other hand, the Leonhardi-2017 EOS

254 shows a remarkable difference when compared to our results at high pressures (Leonhardi and
255 Militzer, 2017). In this case, the difference in input structure should not affect the result as CO is
256 more reactive and can be easily polymerised. The difference between our work and Leonhardi-
257 2017 is hard to understand and must await further clarification.

258 The comparison above indicates that EOSs from classical potentials will suffer from being
259 unable to successfully capture the bonding behaviour of these fluids. This can be understood from
260 the analysis of the evolution of molecular bonding in CO and CO₂ fluids. There is a complex
261 process involving the establishment of new bonds via intermolecular interaction and the
262 decomposition of molecules, which cannot be described by classical models. Moreover, the
263 extrapolation of any experimental data or theoretical calculations may also fail to capture structural
264 changes.



265
266 **Figure 5.** Derived EOS for CO₂ fluid in comparison with existing EOSs. BS-1992 EOS is from
267 Belonoshko and Saxena (1992), CG-2003 EOS is from Churakov and Gottschalk (2003), DZ-
268 2006 EOS is from Duan and Zhang (2006), and FB-2017 is from Fu et al. (2017).



269
 270 **Figure 6.** Derived EOS for the CO in comparison with existing EOSs and data. BS-1991 EOS is
 271 from Belonoshko and Saxena (1991b), Leonhardi-2017 EOS is from Leonhardi and Militzer
 272 (2017).

273

274 4.2 Stability of carbonates at Earth's mantle conditions

275 In order to test the equations of state further, we have used it to predict the decarbonation
 276 reactions of carbonates at high P and T. These reactions are important since carbonates like MgCO_3
 277 and CaCO_3 are the main carbon-bearing minerals in subducting slabs that can be transported down
 278 to the transition zone or lower mantle. Decarbonation reactions do appear to occur, as inferred
 279 from diamonds originating from the mantle transition zone or the lower mantle. The presence of
 280 carbonate inclusions in “super-deep diamonds” indicates that decarbonation reactions may have a
 281 profound influence on mantle structure and the carbon cycle up to lower mantle conditions
 282 (Brenker et al., 2007; Walter et al., 2008). Many experimental and theoretical studies have been
 283 done to investigate the stability of MgCO_3 and CaCO_3 under a wide range of P & T (Drewitt et al.,
 284 2019; Litasov et al., 2008; Litasov et al., 2017; Maeda et al., 2017; Oganov et al., 2008; Santos et
 285 al., 2020; Zhang et al., 2018). However, in-depth analyses are often limited to low pressures due
 286 to the lack of reliable EOSs for CO and CO_2 fluids valid to high P & T. With our CO_2 EOS valid

287 in the P & T ranges of 0-70 GPa and 298.15-4000 K, we investigated the stability of MgCO₃ and
288 CaCO₃ under various conditions.

289 MgCO₃ stabilises in the *magnesite* (*mgs*) phase below ~80 GPa, and above that transforms into
290 *magnesite-II* (Isshiki et al., 2004; Maeda et al., 2017; Oganov et al., 2008). It can decompose into
291 *periclase* MgO (*per*) and CO₂ upon heating. Redfern et al. (1993) applied their EOS for MgCO₃
292 up to 20 GPa and other thermodynamic data to the reaction (**R1**). They found that MgCO₃ is stable
293 over MgO and CO₂ through the mantle, as can be seen in Figure 7a. Fiquet et al. (2002) estimated
294 the stability of MgCO₃ based on their ambient EOS of MgCO₃ and a likely range of $(\partial B_0/\partial T)_p$.
295 As shown in Figure 7a, the equilibrium line of reaction (**R1**) determined by Fiquet et al. (2002)
296 lies below those of Redfern et al. (1993) below ~4 GPa, and goes above those of Redfern et al.
297 (1993) between ~4-16 GPa. $(\partial B_0/\partial T)_p$ does not make much difference below ~10 GPa, and
298 above that the equilibrium line strongly depends on $(\partial B_0/\partial T)_p$. Litasov et al. (2008) determined
299 the EOS of *magnesite* up to 32 GPa and 2073 K. By integrating their EOS and the CO₂ EOS of
300 Belonoshko and Saxena (1991b) in the thermodynamic model, they confirmed the stability of
301 MgCO₃ at mantle conditions. We used the EOSs of MgCO₃ and MgO from Litasov et al. (2008)
302 and the EOS of CO₂ determined above to calculate the Gibbs free energy of reaction (**R1**). As can
303 be seen in Figure 7a, our result agrees well with that of Litasov et al. (2008). It also agrees well
304 with that of Fiquet et al. (2002) below ~10 GPa. The equilibrium lines of Redfern et al. (1993)
305 have a slightly different slope, and this could be due to the use of volume-independent Anderson-
306 Gruneisen parameter. Regardless, MgCO₃ is always found to be stable relative to MgO + CO₂
307 fluid under mantle conditions.

308 The reaction of MgCO₃ with SiO₂ (reaction (**R2**)) was also considered as SiO₂ is a major
309 component in subducted slabs. SiO₂ stabilises mainly in the α -quartz, β -quartz, *coesite* and
310 *stishovite* phases from low to high pressures (Swamy et al., 1994). The product MgSiO₃ also has
311 a rich phase diagram, but the dominant phases are the *orthoenstatite* and *perovskite* phases (Litasov
312 and Shatskiy, 2019; Tomioka et al., 2016). We included all the mentioned structures in the
313 thermodynamic calculation of reaction (**R2**). As can be seen in Figure 7b, our result agrees well
314 with the experimental data at 0–4 GPa. However, the equilibrium line of Litasov et al. (2008)
315 shows a different slope from ours, possibly because they used the CO₂ EOS of Belonoshko and
316 Saxena (1991b), which produces a smaller volume than ours at the same pressure and that stabilises

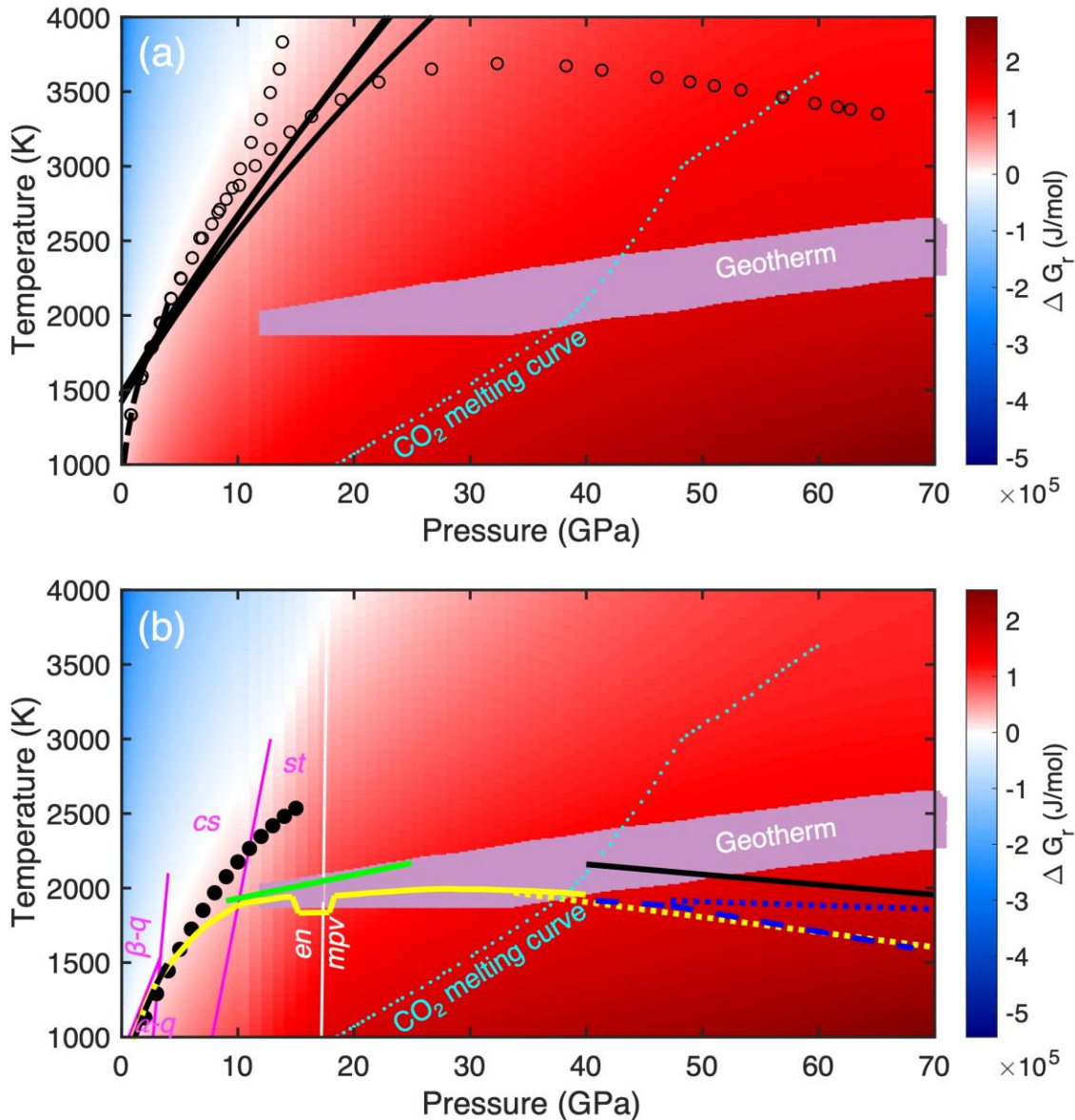
317 CO₂. Nevertheless, these studies suggest the stability of MgCO₃ + SiO₂ over MgSiO₃ + CO₂ fluid
318 under mantle conditions.

319 Figure 7b shows a number of other decarbonation reactions from the literature which are
320 relevant. For instance, above around ~8 GPa, the experiments of Litasov and Shatskiy (2019) (solid
321 yellow line) and Kakizawa et al. (2015) (solid green line) show a change in the slope of the **R2**
322 decarbonation reaction, with it occurring at much lower temperatures than we predict. This is likely
323 due to partial melting of MgCO₃ + SiO₂ occurring before the decarbonation reaction **R2**; however
324 we do not yet model the melts and cannot test this.

325 Recent experiments by Maeda et al. (2017) found that diamond can form from the reaction of
326 MgCO₃ and SiO₂ at deep lower mantle conditions following the reaction



328 Similarly, Drewitt et al. (2019) also find a decarbonation reaction at higher pressures, although not
329 always associated with diamond formation. These conditions lie in the solid region of CO₂ and so
330 are also beyond the predictability of our thermodynamic model. However, the low pressure end of
331 the equilibrium line of (**R5**) determined by Maeda et al. (2017) is predicted to meet the melting
332 curve of CO₂ at *ca.* 40 GPa and 2100 K, where our calculated ΔG_r is *ca.* 140 kJ/mol. This means
333 that reaction (**R2**) cannot occur at *ca.* 40 GPa and 2100 K even if CO₂ is in the solid state, but can
334 only occur further into the solid field where the free energy difference between solid and liquid
335 CO₂ overcomes ΔG_r of (**R2**) shown in Figure 7b. According to the Gibbs free energies calculated
336 by Teweldeberhan et al. (2013), the pressure needs to be ~11 GPa higher than the melting curve
337 for solid CO₂ to be more stable than the fluid by 140 kJ/mol. When considering the uncertainty in
338 the free energies here and in Teweldeberhan et al. (2013), the majority of the high pressure
339 decarbonation reaction of Maeda et al (2017) and Drewitt et al. (2019) are consistent with this.
340 Alternatively, high-pressure decarbonation may be powered by the formation of diamond via CO₂
341 = C + O₂, however, some of the decarbonation reactions seen by Drewitt et al (2019) do not
342 produce diamond. Unfortunately, we do not have suitable equations of state for this reaction to test
343 this. Finally, if MgCO₃ can become unstable in the presence of SiO₂, then MgCO₃ is also expected
344 to be unstable in the absence of SiO₂, given that the Gibbs free energy change is similar for both
345 reactions (**R1**) and (**R2**).



346
 347 **Figure 7.** (a) Gibbs free energy of $\text{MgCO}_3 = \text{MgO} + \text{CO}_2$ calculated using the CO_2 EOS from this
 348 work. Also shown are various phases boundaries from the literature. Black solid curve is the phase
 349 boundary calculated by Redfern et al. (1993) and the black dashed curve is experimental phase
 350 boundary from Litasov et al. (2008). The black open circles are from thermodynamic calculations
 351 of Fiquet et al. (2002), with the ones at higher temperatures using $(\partial B_0/\partial T)_p = -0.021$ GPa/K
 352 and the other ones using $(\partial B_0/\partial T)_p = -0.013$ GPa/K. The CO_2 melting curve (dotted cyan)
 353 determined by *ab initio* simulations is from Teweldeberhan et al. (2013). (b) Gibbs free energy of
 354 $\text{MgCO}_3 + \text{SiO}_2 = \text{MgSiO}_3 + \text{CO}_2$ calculated using CO_2 EOS from this work. The dashed black
 355 curve is the phase boundary from Haselton Jr et al. (1978) and Koziol and Newton (1995). The
 356 filled black circles are from the thermodynamic calculations of from Litasov et al. (2008). Solid
 357 yellow curve is from experiment of Litasov and Shatskiy (2019). Solid green line is from
 358 experiment of Kakizawa et al. (2015). The dashed blue line is from experiments of Drewitt et al.
 359 (2019). The solid black line is from experiment of Maeda et al. (2017). Yellow dotted and blue

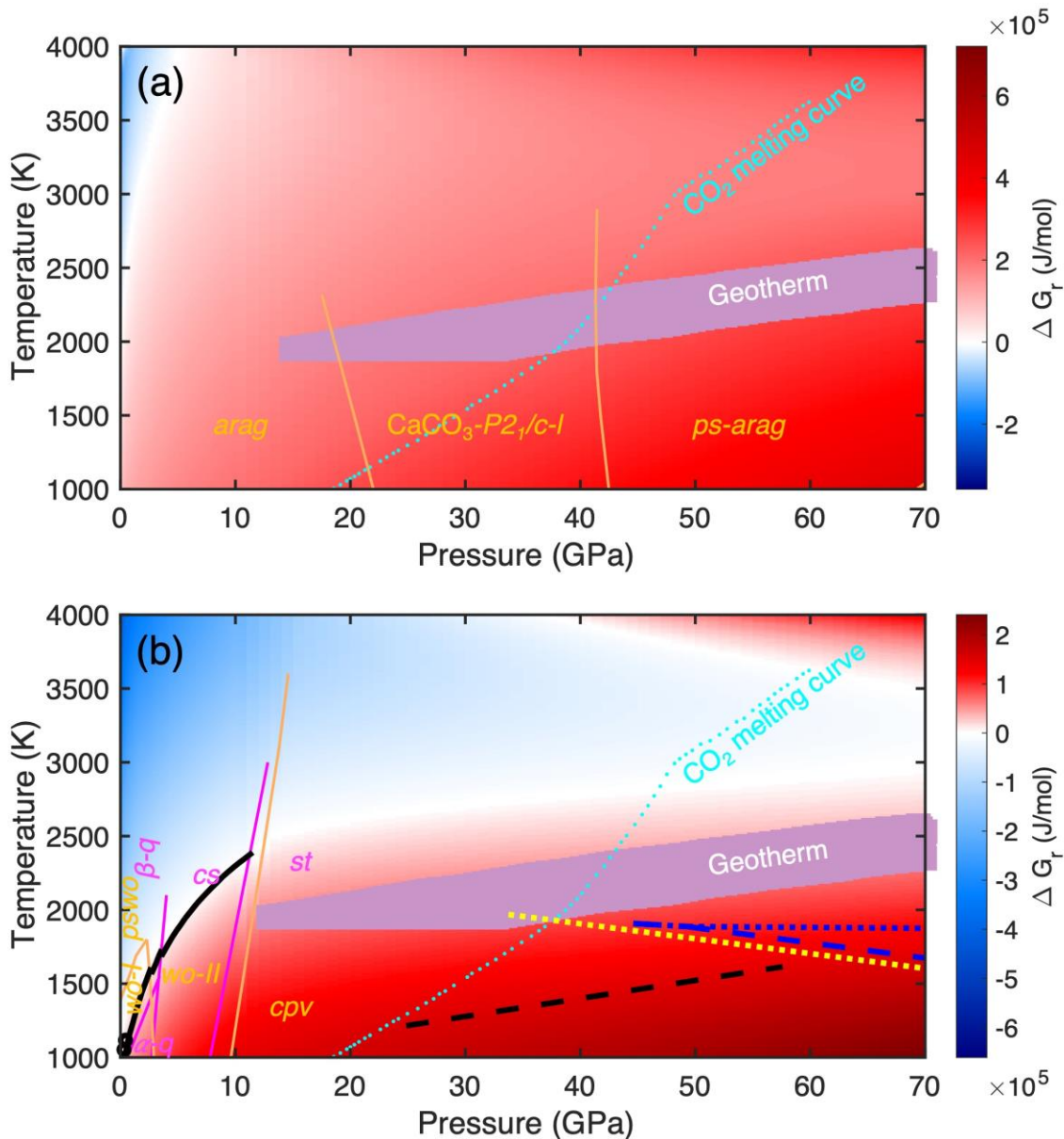
360 dotted lines are the $\text{CO}_2(\text{s}) = \text{C} + \text{O}_2$ boundary from Litasov et al. (2011) and Drewitt et al. (2019),
361 respectively. Magenta lines indicate the calculated phase boundaries for α -quartz (α - q), β -quartz
362 (β - q), coesite (cs) and stishovite (st). The white line indicates the calculated phase boundary
363 between the orthoenstatite and perovskite (mpv) MgSiO_3 .

364

365 CaCO_3 has a complex phase diagram and experiences several phases transformations from low
366 to high pressures. Recently, Zhang et al. (2018) have thoroughly investigated the stability of
367 different polymorphs of CaCO_3 , which include the aragonite, CaCO_3 - $P2_1/c-l$ (l denotes low
368 pressure), postaragonite, CaCO_3 - $P2_1/c-h$ (h denotes high pressure), CaCO_3 - $Pnma-h$, CaCO_3 -VI,
369 and pyroxene-type phases. We also include all these phases in our thermodynamic calculations.
370 For CaO , we considered the quicklime phase. We used the experimental EOS for aragonite and
371 quicklime, and *ab initio* EOS from Zhang et al. (2018) for other CaCO_3 phases. As can be seen in
372 Figure 8a, our result shows that CaCO_3 is stable over $\text{CaO} + \text{CO}_2$ fluid under mantle conditions.
373 The change of Gibbs free energy of reaction (**R3**) along the melting curve of CO_2 is about 200
374 kJ/mol, which is in excellent agreement with *ab initio* calculations of Santos et al. (2019), who
375 calculated the decomposition of CaCO_3 into CaO and solid CO_2 .

376 CaCO_3 is less stable in the presence of SiO_2 , as can be seen in Figure 8b. In the thermodynamic
377 calculation of reaction (**R4**), we considered four stable phases for CaSiO_3 , namely, the
378 wollastonite-I, wollastonite-II, pseudowollastonite and perovskite phases. Our result agrees well
379 with the experimental data at 0-0.5 GPa from Harker and Tuttle (1956) and the thermodynamic
380 calculation of Litasov et al. (2017) up to 12 GPa. Our result together with these studies consistently
381 suggests the stability of CaCO_3 over CaSiO_3 under upper mantle conditions. Recent experiment
382 by Li et al. (2018) observed decarbonation in reaction (**R4**) and suggest that CaCO_3 is unstable in
383 the presence of SiO_2 at conditions from ~25 to 60 GPa and from ~1200 to 1600 K. Such conditions
384 are also in the domain of solid CO_2 and beyond the predictability of our thermodynamic model.
385 Nevertheless, our calculated ΔG_r for reaction (**R4**) along the equilibrium line of Li et al. (2018) is
386 about 150 kJ/mol, which is comparable to our calculated ΔG_r of ~150 kJ/mol for (**R2**) along the
387 experimentally determined equilibrium line of (**R5**); So, it is likely that the transformation of
388 CaCO_3 into CaSiO_3 is also driven by the partial melting of carbonate or by the diamond formation
389 from CO_2 .

390 To summarize this part, our results agree with available experimental and theoretical studies
 391 performed at low pressures. Our results indicate the stability of both MgCO_3 and CaCO_3 pure
 392 phases at upper mantle conditions with or without the presence of SiO_2 . Both MgCO_3 and CaCO_3
 393 may become unstable at deeper mantle conditions, and the decarbonation is likely to be driven by
 394 the formation of diamond or partial melting of carbonate.



395 **Figure 8.** (a) Gibbs free energy of $\text{CaCO}_3 = \text{CaO} + \text{CO}_2$ calculated using our CO_2 EOS from this
 396 work. Orange lines show the phase boundaries between the aragonite (arag), $\text{CaCO}_3\text{-P2}_1\text{/c-l}$
 397 and postaragonite (ps-arag) phases. The CO_2 melting curve (dotted cyan) determined by *ab initio*
 398 simulations is from Teweldeberhan et al. (2013). (b) Gibbs free energy of $\text{CaCO}_3 + \text{SiO}_2 =$
 399 $\text{CaSiO}_3 + \text{CO}_2$ calculated using the CO_2 EOS from this work. Empty back circles are experimental
 400 data from Harker and Tuttle (1956), solid black curve is thermodynamic calculation from Litasov
 401

402 et al. (2017), and the dashed black curve is experimental data from Li et al. (2018). The dashed
403 blue line is from experiments of Drewitt et al. (2019). Yellow dotted and blue dotted lines are the
404 $\text{CO}_2 (\text{s}) = \text{C} + \text{O}_2$ boundary from Litasov et al. (2011) and Drewitt et al. (2019), respectively.
405 Magenta lines indicate the calculated phase boundaries for α -quartz (α -q), β -quartz (β -q), coesite
406 (cs) and stishovite (st). Orange lines show the phase boundaries between the wollastonite-I (wo-I),
407 wollastonite-II (wo-II), pseudowollastonite (pswo) and perovskite (cpv) CaSiO_3 .

408 **5 Conclusions**

409 We have obtained EOSs for CO and CO_2 fluids by performing AIMD simulations, which are
410 valid in the ranges of 1 bar to 40 GPa and 298.15 to 4000 K for CO, and 1 bar to 70 GPa and
411 298.15 to 4000 K for CO_2 . We found that both CO and CO_2 fluids polymerise via the establishment
412 of intermolecular bonding, while the intramolecular bonding is generally unaffected.
413 Polymerisation is found to be a pressure-driven process, starting at very low pressures. These
414 findings suggest a more complex bonding evolution than previously thought, and therefore
415 extrapolations from either low-pressure experimental data or from theoretical calculations using
416 empirical potentials must be treated with caution. The derived CO_2 EOS was applied to
417 decarbonation reactions of both MgCO_3 and CaCO_3 . Our thermodynamic calculations reproduced
418 the experimental results and agree well with other thermodynamic calculations at low pressures.
419 Both MgCO_3 and CaCO_3 pure phases are found to be stable with or without SiO_2 at upper mantle
420 conditions, but they may become unstable approaching the lower mantle.

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424 collaborative facility supplied under the Joint Weather and Climate Research Programme, a
425 strategic partnership between the Met Office and the Natural Environment Research Council. The
426 authors declare no conflicts of interest.

427 **Data availability**

428 The data are already included in the manuscript as Tables 1 and 2.

429 **Appendix A. Supplementary data**

430 Supplementary data to this article can be found online.

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