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1 **Influence of Hydraulic Retention Time, Sludge Retention Time and Ozonation**
2 **on the Removal of Free and Conjugated Estrogens in Japanese Activated Sludge**
3 **Treatment Plants**

4

5

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20

21

Abstract

22 This study describes the occurrence, fate and removal of free estrogens [estrone (E1),
23 17 β -estradiol (E2), estriol (E3), 17 α -ethynylestradiol (EE2)] and their glucuronide
24 and sulphate conjugates [estrone-3-sulphate (E1-3S), 17 β -estradiol-3-sulphate (E2-
25 3S), estriol-3-sulphate (E3-3S), estrone-3-glucuronide (E1-3G), 17 β -estradiol-3-
26 glucuronide (E2-3G) and estriol-3-glucuronide (E3-3G)] in twelve sewage treatment
27 plants (STPs) in Japan. Glucuronide conjugates were only rarely detected in sewage
28 influent and entirely eliminated within the treatment plants. E1 was found at 69 ng/L,
29 E2 at 108 ng/L, E1-3S at 18 ng/L and E2-3S at 78 ng/L in sewage influent. Average
30 removal efficiency for E1, E2 and sulphate conjugates was 88, 92 and 93%,
31 respectively following activated sludge treatment. The removal of E1 and E2 was
32 improved with increasing sludge retention time (SRT), with the highest removal
33 typically found from 12 days SRT onwards. The removal of sulphate conjugates was
34 also related to SRT with highest removals found from 8 days SRT onwards. No
35 correlation was found between hydraulic retention time (HRT) and the removal of any
36 of the estrogens. Ozonation (4-7 mg/L) reduced E3 and E2-3S and E3-3S to below
37 detection levels. Overall ozonation reduced the estrogenicity of the effluent as
38 expressed as estradiol equivalents from 8.4 ng/L to 0.7 ng/L. The results suggest
39 adequate river basin management of estrogens in Japan could be accomplished by a
40 mixture of activated sludge plants with long SRT and where necessary the addition of
41 tertiary ozonation.

42

43 **Keywords:**

44 Free estrogens; Conjugated estrogens; Activated sludge treatment; Sludge retention
45 time; Hydraulic retention time; Ozonation

46 **1 INTRODUCTION**

47 The disruptive impact of steroid estrogens on wild fish and the role played by sewage
48 treatment plants in their discharge is well known [1]. These natural free estrogens
49 have been found to have endocrine disruptive effects on fish even at low ng/L levels
50 [2]. The major source is believed to be the human excretion of free estrogens [2,3].
51 However, the majority of these estrogens are excreted as conjugates with very limited
52 biological activity [4].

53

54 Steroid estrogens in the free de-conjugated state have been detected in sewage
55 treatment plants (STP) discharge waters worldwide [5–11], implying that de-
56 conjugation occurs prior to and/or during wastewater treatment. The conjugated
57 estrogen, depending on the type of attached ester group (glucuronide or sulphate), can
58 potentially de-conjugate back to the active free estrogens [12,13]. For example,
59 elevated levels of estrone (E1) are suspected to arise from transformation of 17 β -
60 estradiol-3-sulphate (E2-3S) into E1 and 17 β -estradiol (E2) in the activated sludge
61 [13]. However, the de-conjugation of glucuronated and sulphated conjugates back into
62 their free estrogenic forms occurs at different rates [12,13]. Thus, the de-conjugation
63 process plays a key role in the overall estrogenic potency of sewage effluents and
64 rivers. There are some studies on the fate of conjugates within sewage treatment
65 plants [7,8], but little is known about the influence of different treatment process
66 parameters on their removal.

67

68 Removal of estrogens in sewage treatment is largely a biological process [14,15] and
69 so differences in this part of treatment will have a large effect on the outcome. Such
70 factors include, temperature, dissolved oxygen concentration, substrate loading rate

71 [16] hydraulic retention time (HRT) and sludge retention time (SRT) [17,18]. A
72 minimum sludge retention time of 10 to 12.5 days has been suggested as the period
73 required for the growth of micro-organisms that decompose E2 and E1 [19]. It is not
74 clear; however, to what extent the conditions which favour the removal of free
75 estrogens influence also the fate of the conjugated estrogens. The two groups of
76 compounds have different physico-chemical characteristics with the free estrogens
77 having relatively high octanol-water partition coefficients of 3-4 Log Kow [5], whilst
78 the conjugated estrogens are highly polar [6,7].

79

80 In Japan, particularly in Kinki area (Shiga, Kyoto and Osaka), sewage systems have
81 mostly employed conventional activated sludge process (CAS) in middle and large
82 scale STPs [20]. The CAS is the most widely used process for the treatment of sewage
83 because of its low operation cost and high performance in Japan. However, the
84 operational parameters (SRT, HRT and Dissolved oxygen) and the treatment steps can
85 differ from one plant to another. To the best of our knowledge, this is the first study to
86 report detail exercise on removal of conjugated estrogens in activated sludge as well
87 as in advanced wastewater treatment process. Twelve activated sludge treatment
88 processes in Kinki area (Japan) were surveyed to investigate the following:

89

- 90 1. The removal of dissolved natural free and conjugated estrogens within the twelve
91 Japanese STPs.
- 92 2. The effect of HRT and SRT on the removal performance of STPs on free and
93 conjugated estrogens.
- 94 3. Effect of ozonation on free and conjugated estrogen reduction.

95

96 2 MATERIALS AND METHODS

97 2.1 Survey in Japanese STPs

98 Twelve activated sludge treatment systems in Japan (Shiga, Kyoto and Osaka) each
99 with slightly different treatment conditions were investigated. A total of 77
100 wastewater samples (influent=28, secondary effluent=28, final effluent=21) were
101 collected from these STPs. The descriptions of each STP and their operational
102 parameters are given in Table 1. It should be noted that the HRT reported here is the
103 biological step contact time only, not that of the whole process. Out of these twelve
104 plants, three STPs use ozonation as a tertiary treatment process followed the
105 conventional and/or advanced activated sludge process. The ozonation contact time
106 were between 12 to 23 min. [Wastewater samples](#) were collected from each STP in
107 three sampling campaigns (November, 2007, November, 2008, and September, 2009).
108 All the plants were sampled in dry weather conditions. The sampling took place at the
109 influent, secondary effluent and effluent stages of the plants concurrently. Population
110 equivalents ranged from 33,900 to 775,500 and the flow rate from 9,500 to 576,265
111 m³/d. The SRT ranges from 3.8 to 22 days with an average of 13 days, whilst the
112 average HRT was 8.7 h (2.4 to 14.1 h).

113

114 Twenty-four hour composite samples were collected using an automatic flow
115 proportional sampler at 4°C. From the sampler, samples were collected in 1 L pre-
116 cleaned amber glass bottles and immediately 1 gram ascorbic acid was added to
117 prevent further biodegradation. All samples were transported to the laboratory in a
118 cooler box maintained at 4°C. The filtration and concentration process of the samples
119 were completed within 24 h of sample collection. [Sludge samples were not analyzed](#)
120 [in this study.](#)

121

122 **2.2 Sample pre-treatment and chemical analysis**

123 The free and conjugated estrogens; E1, E2, estriol (E3), 17 α -ethynylestradiol (EE2),
124 estrone-3-sulphate (E1-3S), E2-3S, estriol-3-sulphate (E3-3S), estrone-3-glucuronide
125 (E1-3G), 17 β -estradiol-3-glucuronide (E2-3G) and estriol-3-glucuronide (E3-3G)
126 were all obtained from Sigma-Aldrich, Japan. The deuterated standards for each
127 compound were obtained from CDN Isotopes. All the chemicals were analyzed by the
128 ultra-performance liquid chromatography coupled to tandem mass spectrometry
129 (UPLC/MS/MS) [21]. The sample pre-treatment development has been described in
130 some detail previously [21]. Briefly, samples were first filtered with GF/B glass fibre
131 filter (1 μ m pore size; Whatman, UK). After adding the appropriate amount of all the
132 deuterated surrogates, solid phase extraction (SPE) with Oasis HLB (200 mg, 6 cc; 30
133 μ m partial size, Waters, UK) cartridges was performed. The SPE cartridges were
134 dried for 1 h under the gentle air pressure in a glass manifold. A Sep-Pak Plus NH₂
135 (360 mg, aminopropyl, 55–105 μ m partial size, waters) cartridge was connected
136 below the dried Oasis HLB cartridge to reduce the effect of sample matrix on
137 ionization.

138

139 Free estrogens were eluted first from the cartridge using methanol, followed by 0.5%
140 NH₄OH methanol to elute the conjugated estrogens [21]. Chromatographic
141 separations were carried out on a Waters Acquity UPLC system (Milford, MA) using
142 an Acquity BEH C8 column (100 mm, 2.1 mm, 1.7 μ m particle size) for free and
143 Acquity BEH C18 column (50 mm, 2.1 mm, 1.7 μ m particle size) for conjugated
144 estrogens. Separation was performed with a binary mobile phase (acetonitrile: milli
145 Q) at a flow rate of 0.2 mL/min [21]. UPLC/MS/MS with electrospray ionization in
146 the negative ionization mode was used in this study. The method parameters are

147 shown in the Supporting Information (Table S1). The detection limits of studied
148 estrogens were between 0.2 (sulphate conjugates) and 0.8 ng/L (E3-3G). Recovery
149 rates of each deuterated surrogates were between 65 (E2 in influent) and 108% (E1-3S
150 in influent) (Table S2).

151

152 **(Insert Table 1)**

153

154 **2.3 Removal calculations**

155 Percentage removal of estrogens during sewage treatment is used as a collective term
156 to describe the disappearance of chemicals from the effluent due to processes such as
157 biodegradation and sorption on sludge. The degree of removal obtained was
158 calculated from the total analyte concentration in raw sewage water (C_{in}) and effluent
159 (C_{out}) according to Eq. 1:

$$160 \quad \text{Removal (\%)} = \frac{(C_{in} - C_{out})}{C_{in}} \times 100 \quad (1)$$

161 Statistical analysis was performed by using commercially available statistical software,
162 Statistica (Statsoft, Tulsa, OK, USA).

163

164 **2.4 Estradiol equivalents (E2 equiv) calculations**

165 To address the estrogenic potency for a mixture of natural estrogens (E1 and E2) in
166 terms of E2 equiv was calculated as follows [22].

$$167 \quad \text{E2 equiv} = [E2] + [EE2] \times 10 + [E1]/3 \quad (2)$$

168 These E2 equiv values were used for the investigation of the impact of SRT and
169 ozonation in the removal of estrogenic activity within the STPs.

170

171

172 **3 RESULTS AND DISCUSSION**

173 **3.1 Occurrence of free and conjugated estrogens in the wastewater samples**

174 Among the free estrogens, E2 was detected in the range of 5 to 108 ng/L (36 ng/L
175 mean) in influent samples but was detected only in few secondary effluents (up to 9
176 ng/L) samples. E1 was detected in the range of 11 to 69 ng/L (30 ng/L mean) in
177 influent, and 1 to 36 ng/L (3 ng/L mean) in final effluent samples (data not shown).
178 High effluent concentration may reflect de-conjugation of conjugated metabolites
179 during the treatment process[13]. Reported E1 and E2 concentrations are in
180 accordance with previous observations [21,23,24]. E1 values were similar to the
181 previously reported concentrations in Japanese STP, where a range of 66 ng/L
182 (Influent) and 80 ng/L (effluent) was reported. Synthetic estrogen EE2 was never been
183 detected in any sample. This is not unexpected as it is still not a popular method of
184 contraception in Japan [20]. E3 was detected only in influent sample (64 ng/L mean),
185 implying a ready biodegradability during the sewage treatment process.

186

187 **(Insert Figure 1)**

188

189 The glucuronide conjugates were found in only two influent samples where E1-3G
190 was found at 3.7 ng/L and E2-3G at 3.5 ng/L concentration. In a previous study, E1-
191 3G was detected at 5 ng/L, E2-3G at 4.0 ng/L and E3-3G at 19.0 ng/L in three UK
192 STPs influents [8]. However, D'Ascenzo et al, [25] failed to detect E3-3G, but
193 reported E2-3G at 5.0 ng/L and E1-3G at 4.0 ng/L (mean concentration) in six Italian
194 activated sludge plant influents. Sulphate conjugates were frequently observed in
195 these Japanese STPs influents and secondary effluents (Figure 1) with E2-3S reaching
196 up to 78.0 ng/L (mean concentration 19.4 ng/L) in the influent. E1-3S was detected in

197 influent and few secondary effluent samples at a mean concentration of 8 ng/L (0.8 to
198 18 ng/L) and 3.4 ng/L (<0.2 to 4.4 ng/L), respectively. This is similar to a previous
199 survey in an STP in Japan where a range of 7.7 ng/L (E1-3S) and 36.1 ng/L (E3-3S)
200 in the influent were reported [7]. In an another study in Japan, E1-3S was detected
201 upto 2.2 ng/L in STP effluent and 0.3 to 0.9 in different river and lake water samples
202 [26]. E3-3S was never been detected in any effluent samples, however it was detected
203 upto 19 ng/L in influent samples.

204

205 **3.2 Effect of SRT on estrogen and conjugates removal**

206 The E1, E2 and E2 equiv (Eq. 1) removal efficiencies were assessed and compared for
207 each of the STPs in the survey. Results denoted that the longer SRT achieved highest
208 estrogen removal and E1 took longest time to be eliminated completely. Concurrently,
209 there did appear to be a significant relationship ($p<0.05$) between SRT and the
210 removal of free estrogens (Figure 2). The highest removal rates could be found from
211 12 d SRT onwards. Mean removal rates of more than 84 and 98% were observed for
212 E1 and E2, respectively, at SRT higher than 12 days. In addition, consistent removal
213 for studied estrogens was observed over 18 days SRT. [Previously, more than 90%
214 removal was observed for natural estrogens at SRT of 12-15 days, however in the
215 membrane bioreactors with nitrification and denitrification processes \[15\].](#) Whilst,
216 mean removal was 65% for E1 and 85% for E2, at SRT lower than 12 days. This is
217 not to say that SRT periods greater than 12 d guaranteed high removal, but that the
218 highest removal rates were most likely to occur in plants beyond this sludge age.
219 There also seemed to be a significant relationship ($p<0.05$) between SRT and removal
220 of the sulphate conjugates, E1-3S ($r^2=0.36$) and E2-3S ($r^2=0.42$). However, in this

221 case the highest removals appeared to be from 8-9 d SRT onwards (more than 99%
222 removal).

223 **(Insert Figure 2)**

224 A high sludge age will provide a greater opportunity for slow growing
225 microorganisms to establish themselves on the sludge flocs and these have been
226 linked to estrogen biodegradation [15,27]. It seems that species capable of degrading
227 E2 are relatively common in activated sludge [28,29] but this is not the case for E1.
228 However, there is evidence that specialist nitrifying bacteria can degrade E1 and these
229 are favoured by long sludge ages [30,31]. These results imply that increasing sludge
230 age with their attendant bacteria also encourages sulphate conjugate degradation.
231 Recent microcosm studies suggest that a significant proportion of E2-3S can be
232 transformed to the free E1 hormone [13].

233

234 **3.3 Effect of HRT on estrogen and conjugates removal**

235 The HRT in the 12 STPs varied from 7 h to 14 h. No relationship between HRT on the
236 removal of the estrogens and their sulphate conjugates was visible (Figure 3). Positive
237 correlation with SRT and not with HRT could be explained by sorption of free
238 estrogens on the sludge. In terms of polarity, free estrogens [$\log K_{ow}$ between 2.45
239 (E3) to 4.01 (EE2)] would be considered as moderately hydrophobic compounds [5]
240 and the higher proportion of sorption to sewage particles in wastewater might be
241 expected. However, in case of more hydrophilic sulphate conjugates, bacteria and
242 enzymes can hydrolyze these to yield the free estrogens particularly in activated
243 sludge process [13]. Similar results were reported by Gomes et al, [12], however,
244 using a slightly different media (artificial activated sludge) in a microcosm study.

245 **(Insert Figure 3)**

246 **3.4 Ozonation and ecotoxicological risk assessment**

247 The STPs; B, C and G having ozonation as a tertiary treatment process were examined
248 in 6 sampling campaigns (Table 2). For these STPs the average E2 equiv removal
249 efficiencies from the influent samples was almost 96% (Table 2). As far as
250 ecotoxicological risk is concern, ozonation reduced the estrogenicity of the effluent as
251 expressed in E2 equiv from 8.4 ng/L to 0.7 ng/L. This indicates that ozonation could
252 reduce the E2 equiv below the threshold (1 ng/L) to cause endocrine disruption to
253 aquatic organisms [22], as 1 ng/L E2 equiv level in the UK is taken as a trigger level
254 for vitellogenin (VTG) production in male fish. Except on one occasion (E1-3S, 0.5
255 ng/L), sulphate conjugates were never detected in effluent samples having ozonation
256 as a tertiary treatment. Previously, ozonation has been found extremely efficient at
257 removing estrogens from the wastewater treatment plants [32,33].

258

259 **(Insert Table 2)**

260

261 **4 CONCLUSIONS**

262 Occurrence and removal of the estrogens and their conjugates were investigated in
263 twelve STPs in Japan. This study demonstrated that sulphate conjugates are readily
264 degraded in Japanese STPs with their removal promoted by longer SRT periods. The
265 HRT of an activated sludge plant had no bearing on its estrogen removal efficiency.
266 On a practical level, this survey suggests that where estrogen removal performance is
267 under consideration, then an SRT above 12 d is desirable, with above 18 d being
268 particularly effective. Ozonation has proved to be particularly effective in estrogen
269 removal whilst conventional activated sludge plants being sufficiently effective with
270 longer SRTs.

271

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280

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391 **Figure Captions**

392

393 Figure 1 Concentration (mean) of free and conjugated estrogens in 12 activated sludge
394 treatment plants in Japan (n=28); error bar shows range of the detection.

395

396 Figure 2 Correlation plot of SRT against the E1, E2, E2 equiv, E1-3S and E2-3S
397 removal for 12 Japanese STPs (n=28).

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399 Figure 3 Correlation plot of HRT against the E1, E2, E2 equiv, E1-3S and E2-3S
400 removal for 12 Japanese STPs (n=28).

Table 1 Detailed description of the surveyed STPs in Japan (Kyoto, Shiga and Osaka)

ID	Treatment	Physicochemical	HRT (h)	SRT (Day)	Sampling Time	Flow (m3/d)	Served population	
A	A-1 CAS with coagulation	Chlorination	5.6	18.4	2007/11	57,000	99,000	
	A-2 AO with carrier		2.8	14.2	2008/12			
B	B-1 Step AO	Ozonation(4.3mg/L)	9.9	22	2007/11	65,210	84,000	
	B-2 Pure O2		4.6	9.5	2008/11			
C	CAS; AO	Ozonation(7.4 mg/L)	9.8	8.3	2007/11 2008/11	92,280	146,500	
D	D-1 CAS;AO;A2O;stepAO	Chlorination	12.1	19	2007/11	576,265	775,500	
			D-2	11.6	16			2008/11
			D-3	9.4	18			2009/9
E	AO with coagulation stepAO with coagulation	Chlorination	10.9	17	2007/12 2008/12	50,000	236,000	
F	AO with coagulation stepAO with coagulation	Chlorination	14.1	13.1	2007/12 2008/12	9,500	33,900	
G	AO with coagulation A2O with coagulation stepAO with coagulation	Ozonation	9.4	12	2007/12 2008/12	200,000	604,000	
H	AO with coagulation stepAO with coagulation	Chlorination	9.9	13	2007/12 2008/12	39,000	110,000	
I	CAS	Chlorination	7.0	16	2008/11	87,140	210,400	
J	J-1 CAS(quasi-AO)	Chlorination(1.4mg/L)	6.5	6.7	2009/9	191,276	263,137	
	J-2 CAS	Chlorination(2.0mg/L)	7.0	3.8				
K	AO	Chlorination(2.7mg/L)	8.6	5.0	2009/9	160,544	158,018	
L	AO	Chlorination(1.4mg/L)	8.4	6.3	2009/9	135,833	210,108	

CAS= conventional activated sludge

AO = anoxic/oxic

A2O = anaerobic/anoxic/oxic

Step AO = anoxic/oxic/anoxic/oxic

Table 2 Estradiol equivalent (E2 equiv) and sulphate conjugates concentrations (ng/L) in sewage treatment plants samples having ozonation process as a tertiary treatment.

	Sampling event	STP B1			STP C			STP G		
		Inf.	S. Eff.	Eff.	Inf.	S. Eff.	Eff.	Inf.	S. Eff.	Eff.
E2 Equiv	1 st	18.4	6.2	1.7	37.5	9.1	0.7	122.1	10.8	1.2
	2 nd	14.1	10.6	ND	31.3	7.4	ND	93.1	6.1	0.4
E1-3S	1 st	3.2	ND	ND	4.7	ND	ND	11.2	3.2	0.5
	2 nd	1.6	ND	ND	5.2	ND	ND	7.8	ND	ND
E2-3S	1 st	1.8	ND	ND	9.2	ND	ND	61.5	0.8	ND
	2 nd	2.3	ND	ND	8.3	ND	ND	41.0	0.4	ND
E3-3S	1 st	6.2	ND	ND	17.9	ND	ND	10.9	0.3	ND
	2 nd	8.2	ND	ND	18.7	ND	ND	9.2	0.3	ND

ND= Not Detected; Inf.= Influent; S. Eff.= Secondary Effluent; Eff.= Effluent

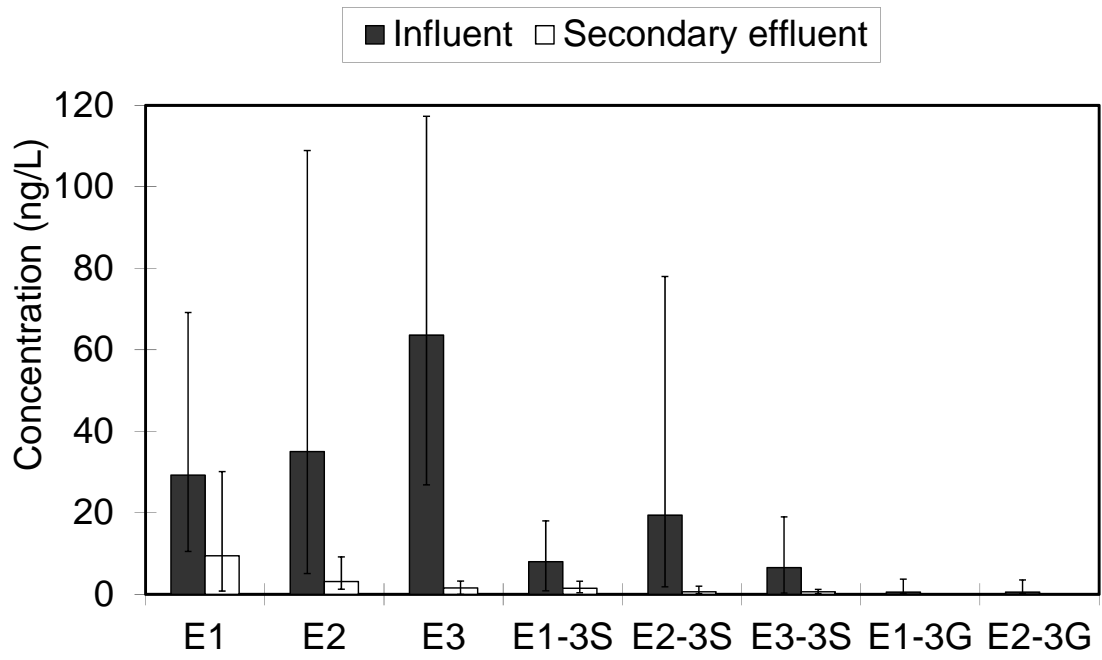


Figure 1 Mean concentration of free and conjugated estrogens in 12 activated sludge treatment plants in Japan (n=28); error bar shows range of the detection.

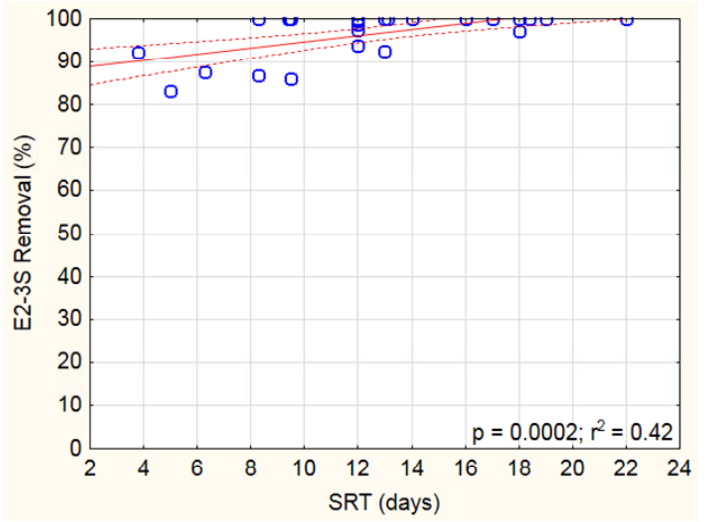
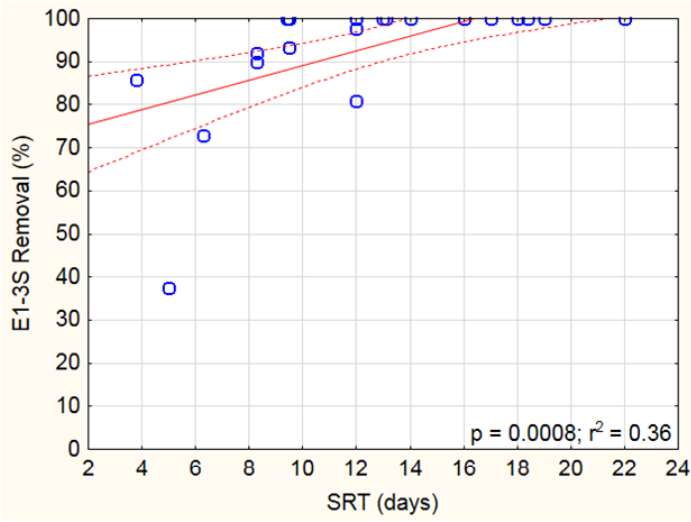
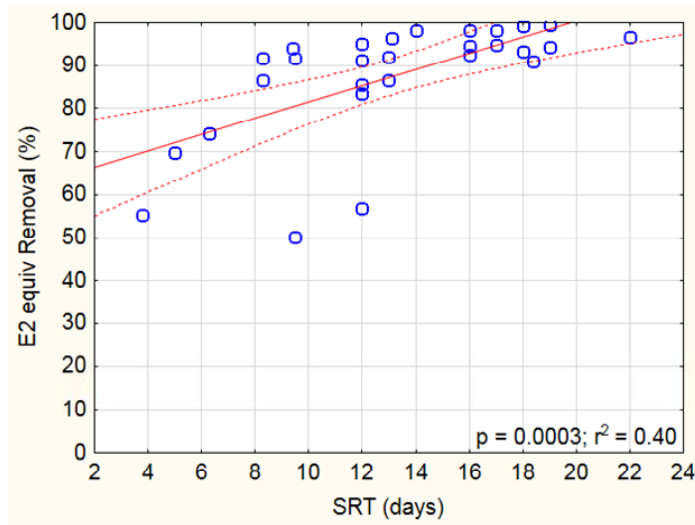
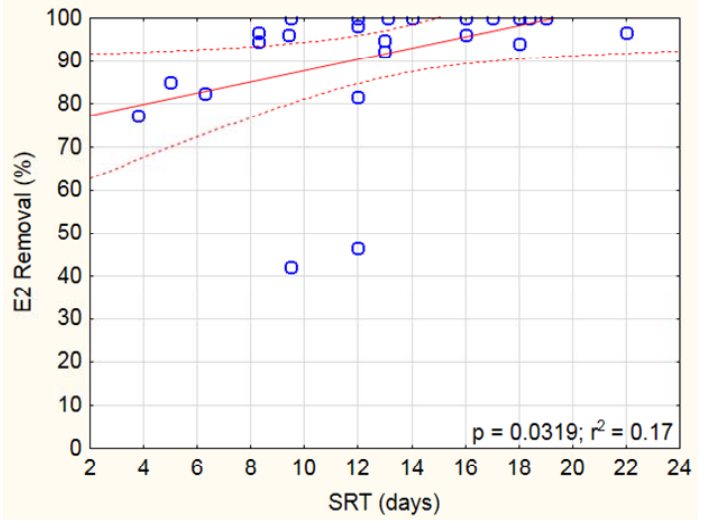
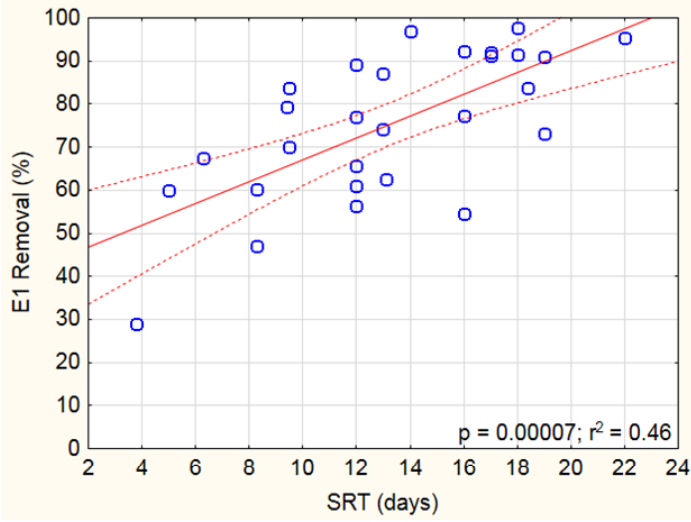


Figure 2 Correlation plot of SRT against the E1, E2, E2 equiv, E1-3S and E2-3S removal for 12 Japanese STPs (n=28).

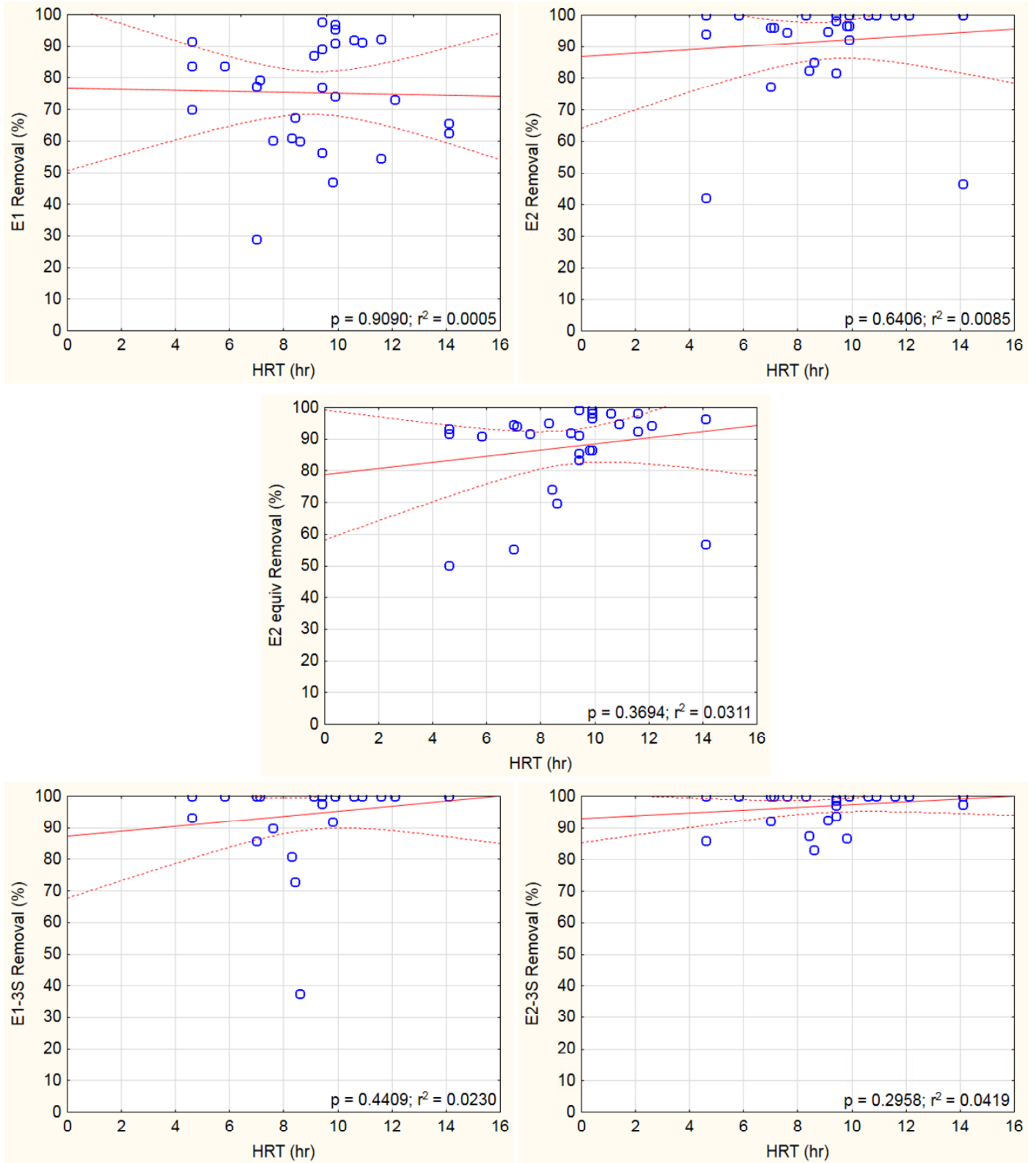


Figure 3 Correlation plot of HRT against the E1, E2, E2 equiv, E1-3S and E2-3S removal for 12 Japanese STPs (n=28).