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Assessing Options for Remediation of Contaminated 5

- Mine Site Drainage Entering the River Teign, 6
- Southwest England 7

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13 Abstract: The river Teign in Devon has come under scrutiny for failing to meet Environmental 14 Quality Standards for ecotoxic metals due to past mining operations. A disused mine known as 15 Bridford Barytes mine, has been found to contribute a significant source of Zn, Cd and Pb to the 16 river. Recently, studies have been focused on the remediation of such mine sites using low-cost 17 treatment methods to help reduce metal loads to the river downstream. This paper explores the 18 metal removal efficiency of red mud, a waste product from the aluminium industry, which has 19 proven to be an attractive low-cost treatment method for adsorbing toxic metals. Adsorption 20 kinetics and capacity experiments reveal metal removal efficiencies of up to 70% within the first 2 21 hours when red mud is applied in pelletized form. Also, it highlights the potential of biochar, 22 another effective adsorbent observed to remove >90% Zn using agricultural feedstock. Compliance 23 of the Teign has been investigated by analysing dissolved metal concentrations and bioavailable 24 fractions of Zn to assess if levels are of environmental concern. By applying a Real-World 25 Application Model, this study reveals that compressed pellets and agricultural biochar offer an 26 effective, low-cost option to reducing metal concentrations and thus improving the quality of the 27 river Teign.

- 28 Keywords: trace metals; mine remediation; zinc; red media; biochar
- 29

30 1. Introduction

31 Historic mining in the southwest of England has left a legacy of environmental and socio-32 economic impacts. Whilst mining operations have largely ceased throughout Devon and Cornwall, 33 impacts have persisted resulting in localised contamination and elevated metal concentrations in 34 soils, sediment, and waters. In England, pollution from mine waste affects over 1,700km of rivers [1] 35 with the potential to reduce the quality of drinking water and threaten sensitive aquatic ecosystems. 36 This legacy presents a challenge in achieving the requirements set out by the Water Framework 37 Directive (WFD) (Directive 2000/60/EC) which has established Environmental Quality Standards 38 (EQS) for specific pollutants such as arsenic (As), zinc (Zn), copper (Cu), iron (Fe), chromium (Cr) 39 and manganese (Mn), Priority Substances such as lead (Pb) and Priority Hazardous Substances such 40 as cadmium (Cd). Meeting the standards and protecting the quality of our water bodies is therefore 41 of fundamental importance.

42 The river Teign, sourced in Dartmoor, Devon, is at risk of not meeting the requirements set out 43 by the WFD and forms the focus of this study. Exploitation of mineral resources at a local disused 44 mine in Bridford, known as Bridford Barytes mine, have contributed to elevated concentrations of 45 potentially toxic metals. Mining for baryte (barium sulphate) took place between 1855 and 1958, 46 however prior to this, Pb-Zn mining occurred within the catchment ^[2]. Both episodes have been 47 responsible for releasing potentially ecotoxic metals into the river Teign and monitoring data has 48 consistently shown exceedances in metal concentrations, particularly Zn which presents the basis for 49 this investigation.

50 Metals sourced from mining operations are typically discharged from mine adits, where Acid 51 Mine Drainage (AMD) is generated releasing trace metals into the environment with potentially 52 adverse effects on the ecology. AMD is produced when sulphide-bearing minerals released from 53 mining activities are exposed to atmospheric conditions. The most common sulphide mineral in this 54 process is pyrite (FeS₂). The oxidation of pyrite leads to the generation of sulphate and an increase in 55 proton acidity ^[3], this reaction is responsible for considerable increases in acidity within the natural 56 environment. Due to this increase in acidity, pH associated with AMD is typically below 4.0 ^[4], in 57 which metals are highly soluble and easily mobilised, commonly these metals include Mn, Cr, Cd, 58 Zn, Pb and As.

59 Zn is one of the most encountered WFD specific pollutants from mining activities. It is a metal 60 both essential and toxic to organisms, monitoring the concentration of Zn at the catchment scale is 61 therefore critical to help sustain and preserve the environment. Notably, Zn is often present in high 62 concentrations due to the background geology; this presents unique complications in assessing the 63 risk of impacts. However, studies have shown that Zn in sediments of the river Teign and estuary are 64 not entirely naturally occurring and are derived from mining pollution ^[2]. These elevated levels of Zn 65 have been attributed to the episodes of Ba and Pb-Zn mining throughout the Teign catchment 66 including a major source at Bridford Barytes mine. In catchments affected by AMD, Zn is commonly 67 present in its most ecotoxic form Zn²⁺, as is the case with the river Teign. The release of this hydrated 68 Zn ion into the environment is toxic to aquatic biota at elevated concentrations, with reports of 69 reproductive and developmental responses in fish and other aquatic organisms ^[5]. With regards to 70 human health, long term excessive exposure has been identified as a contributing factor to chronic 71 diseases, a decrease in immune system function and even infertility [6.7]. Preventing such adverse 72 effects to aquatic life and human health is the driving force behind environmental legislation.

73 Over the years, growing concern for the environment and human health has led to an increase 74 in legislation governing pollution associated with the mining industry. The WFD has become one of 75 the most influential pieces of EU law concerning water pollution and the quality of our water bodies. 76 The directive is built upon the principles of sustainable development and requires the development 77 of management strategies referred to as River Basin Management Plans (RBMP). It also requires 78 member states to classify the ecological quality of waters once every 6 years as either high, good, or 79 moderate; with pass/fail Environmental Quality Standards (EQS) for chemicals of concern. To achieve 80 good status, all the chemical and ecological parameters have to be 'good' as it is a one out-all out 81 assessment. Currently the lower Teign catchment only achieves 'moderate' status for failing to meet 82 the standards required for good ecological classification and for periodic failures of the Zn EQS [8]. 83 Consequently, understanding the contribution of Zn to this river catchment and undertaking 84 appropriate mitigation is key to meeting the demands of the WFD and is the rationale behind this 85 study.

86 The EQS established by the WFD are based upon recommendations from the United Kingdom 87 Technical Advisory Group (UKTAG) and are monitored closely by the Environment Agency. They 88 are derived from present scientific understanding of the conditions needed for a healthy water 89 environment and utilise ecological data from thousands of sites across the UK. The revised standard 80 for Zn in freshwaters is currently 10.9 µg/l bioavailable plus the ambient background concentration 91 2.9 µg/l ^[9]. Importantly, the chemical form of zinc is greatly influenced by the hydrological and 92 physiochemical conditions of the water ^[10]. Metal-concentrations, pH conditions and amount of 93 organic matter all control the bioavailability and toxicity of zinc ^[11], not considering the bioavailable
94 fraction of zinc may result in an under or over estimation of the risks posed by the metal. These
95 influences are therefore an important consideration when assessing if a water body is in fact 'failing'
96 due to the presence of the metal and is consequently an environmental concern.

97 Practical and cost-effective treatment for mine water is topical and extensive research has been 98 undertaken to assess the application of different treatment methods in the UK. The degree of 99 environmental pollution generated by AMD is highly variable, meaning treatment must be flexible 100 and specific to each site. Passive methods to remove heavy metal ions are currently favoured due to 101 their low cost and local availability, with techniques including constructed wetlands, limestone for 102 neutralisation, precipitation, and adsorption ^[12]. Biochar is an attractive, low-cost, adsorbent material 103 whose adsorptive properties can be influenced by the type of feedstock used. The remediation 104 potential of biochar has been noticed by previous studies ^[28,29], with focus on the effects of pyrolysis 105 temperature, contact time, initial metal concentration and type of feedstock used. It has been found 106 that agricultural biochars have high adsorption capacities (11000mg/kg) compared to wood biochars 107 (395.8mg/kg) [23,24]. This study emphasizes the significance of using different biochar feedstock and 108 their influence on the removal of Zn, Cd and Pb.

109 Red Media Technology has been trialing the capability of 'Red Mud' (RM) for adsorbing heavy 110 metals from discharged mine waters at a relatively low cost. Millions of tonnes of hazardous RM 111 waste is produced each year as a by-product of the aluminium industry; the utilization of this 112 material therefore supports the concept of waste-recycling. It is a highly alkaline material with a pH 113 of 10-13, the red colour comes from the presence of oxidised iron which comprises up to 60% of the 114 mass of the product ^[18]. The RM is in pellet form, pre-treatment of the pellets via heat and acid 115 treatment has been found to increase adsorption and the removal efficiency of heavy metals ^[19]. 116 Laboratory studies have investigated the capabilities of four different types of pellet which have 117 undergone treatment: Compressed (CP), fired (FP), fired-acid-etched (FAE) and a new powdered 118 pellet (PP). Importantly, studies have shown that the pre-treatment of pellets is essential in the 119 adsorption process and hence determines the overall effectiveness of removing heavy metals from 120 mine water [14]. However, they seldom consider the practicalities of applying these treatment methods 121 to a real-world application. This report aims to evaluate the feasibility of red mud pellets and biochar 122 as treatment methods, weighing up the benefits and costs to see which method will be most 123 applicable for reducing metal loads to the Teign. Principally it focuses on Zn, however the removal 124 efficiencies for the priority substances Cd and Pb have also been considered for comparison.

125 Compressed pellets have been tested in the laboratory and during a field scale trial by Hill (2016) 126 ^[14] and Comber (2015) ^[16] respectively. CP have been compacted under high pressure, forming small 127 and crumbly pellets of varying sizes (Figure 1a) [14]. They have lost porosity during compaction and 128 have a high surface area; however, the field trial shows that the pellets lack structural integrity and 129 suffered degradation during the experiment ^[16]. Lab based experiments using fired pellets have been 130 conducted by Hill (2016) ^[14] and Turner (2017) ^[13]. Production of the FP involves heating in a kiln at 131 1050°C for 2 hours and allowed to cool for a further 2 days [14]. The pellets are more uniform in size, 132 with a coarse texture and an overall lower surface area compared with the compressed pellets (Figure 133 1b) [13]. The adsorption efficiency of the fired acid etched pellets have been tested by Turner (2017) [13], 134 where they are described as small, bright orange pellets with a powdery texture and a smoother 135 surface produced from etching (Figure 1c). The powdered pellets described by Turner (2017)^[13], are 136 similar in appearance to the compressed pellets, with a cylindrical shape, powdery texture, and a

137 dark orange colour, fired at 800°C.

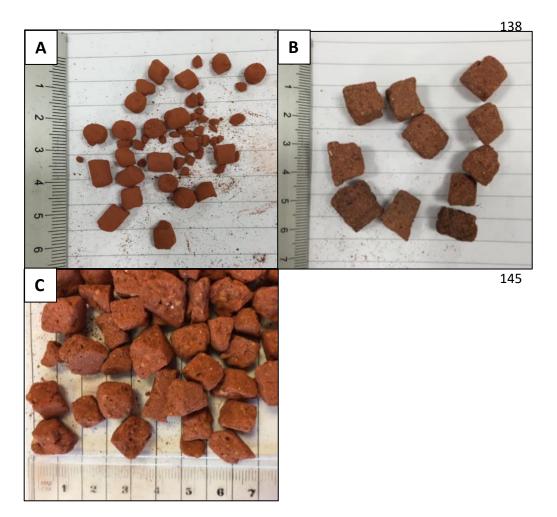


Figure 1. Red media pellets which have all been pre-treated. (A) Compressed Pellets ^[14]. (B) Fired
Pellets ^[14]. (C) Fired acid etched pellets ^[13].

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155 Ultimately, information collated on these studies of different treatment methods are employed 156 by the competent authorities (Environment Agency and Coal Authority) to develop and build mine 157 water treatment schemes to clean up our waters where the quality has been compromised by 158 pollution from abandoned mine sites ^[1]. Currently, one of the greatest challenges in treating pollution 159 generated from AMD is finding a method that meets the expectations of efficiency, cost, and 160 sustainability. The objective of this study is to assess the necessity of Zn, Cd and Pb removal in the 161 river Teign and evaluate the efficiency of treatment methods that utilise red media. The results will 162 enable an assessment of the practicalities associated with reducing Zn loads to the catchment, and an 163 overall more comprehensive understanding of adopting low-cost adsorption treatments to mine sites 164 in the UK.

165 2. Methodology

166 *2.1. Study Area*

167 The study is based on a former baryte mine in Bridford, situated south west of Exeter 168 (SX83148643). The mine is located within the Teign valley on the north eastern edge of Dartmoor 169 (Figure 2) where metalliferous mineral deposits have been extracted since the bronze age due to the 170 presence of a large granite batholith. Mineral deposits in the area consist mainly of shales, mudstones, 171 cherts and tuffs, also known as the Culm measures; these deposits contain the Ba-Pb-Zn loads ^[15].

- Initially, Pb mining took place at the site dated at around 1804, however, low profits moved
 production to Ba in 1855, with final abandonment of the mine in 1958 ^[2,16].
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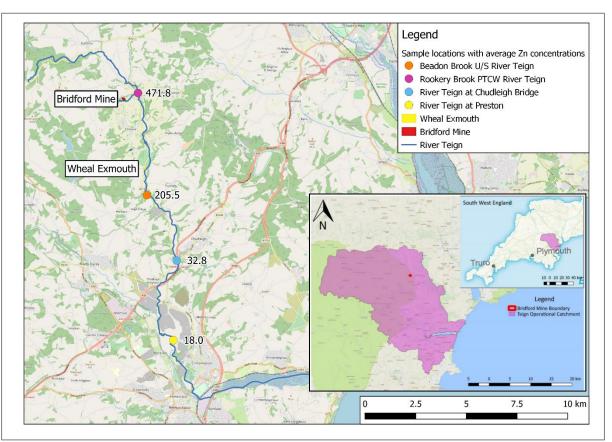


Figure 2. Map showing the location of Bridford baryte mine which is situated on the north eastern edge of Dartmoor within the Teign catchment along with the Environment Agency sampling points and mean zinc concentrations (μg/l) (2000-2020 data).

178 Mine water discharged from the main adit is channelled to the Bridford beck via an Environment 179 Agency monitoring point. The Bridford beck is a tributary of the Rookery Brook sourced in Dartmoor 180 which flows downstream approximately 1 km into the river Teign, both water courses currently 181 exceed the Zn EQS ^[14,16]. However, these tributaries comprise a small area of the catchment 182 (approximately 6km² out of 540km² for the Teign catchment ^[17]) and at first instance, seem unlikely 183 to contribute greatly to the elevated Zn concentrations of the Teign.

184

185 2.2. Current studies using Red Media Technology products

186 Laboratory studies have been undertaken to assess the removal efficiency of pre-treated pellets 187 ^[13,14]. Samples were collected from the adit outflow in June and November 2016 at Bridford along with 188 in situ measurements of pH, temperature, dissolved oxygen content and redox potential. Previous 189 monitoring has shown concentrations of trace metals in the adit discharge to be remarkably stable 190 over time. CP, FP, FAE and PP were supplied by Red Media Technologies to determine their metal 191 removal efficiency and suitability to a mine environment ^[20]. An adsorption kinetics experiment 192 tested the rate of analyte adsorption by adding 850ml of mine water to 200g of RM pellets in a 1 litre 193 polythene bottle followed by continuous agitation on an orbital shaker, with 9ml of sample being 194 remover by syringe at set time intervals which were filtered through cellulose nitrate 22mm 195 membranes before preservation using ultra pure nitric acid (100 µl of 20% acid). A full outline of this 196 methodology can be found in the Electronic Supporting Information (ESI, S1). Starting and final 197 analyte concentrations of the mine water were analysed using Inductively Coupled Plasma 198 instruments such as ICP-MS (Inductively Coupled Plasma – Mass Spectrometry, Thermo Scientific X 199 Series 2, with indium and iridium internal standards) and ICP-OES (Inductively Coupled Plasma – 200 Optical Emission Spectrometry; Thermo Scientific ICAP 7400 Series with yttrium internal standard), 201 the removal efficiencies were then calculated after 2 hours for Cd, Pb and Zn. Briefly, ICP-OES was 202 used for samples with metals in the mg/l range and ICP-MS for metals in the μ g/l range. Certified 203 Reference Materials (Enviromat, EPL-3), internal control samples and blanks were determined within 204 each batch of samples to ensure data quality. Recoveries for Zn, Pb and Cd were 100% +/- 10% and 205 precision for the 3 replicate analyses for each sample were typically less than 5% relative standard 206 deviation [13,14]. The pH was also tested at the start and end of the experiment to reveal any 207 neutralising capabilities of the pellets [13].

208 As well as a kinetics experiment, an adsorption capacity column experiment was undertaken to 209 determine the adsorption behaviour and optimum capacity of the CP and FP in mg of metal 210 sorbed/kg of media used. Depending on the amount of RM material available columns were either 211 clear polycarbonate with approximately 1 litre capacity or a 60ml polythene syringe. The columns 212 were bunged at either end with fittings to accept 1.5mm diameter polythene tubing from a Gilson 213 Miniplus 3 peristaltic pump. The columns (3 replicates) were packed with test material and mine adit 214 water passed through at a rate of typically 1ml/min. adit water exiting the column was collected (9ml) 215 filtered and preserved as per the kinetic experiment. The adsorption capacity was calculated using 216 the starting concentrations of the elements, the amount of solution which had flowed through them 217 and the weight of pellets within the column (ESI, S2). The highest capacity achieved for each metal 218 has been recorded [14].

219 A field scale trial of the removal efficiency of toxic metals using the pellets was undertaken by 220 Comber (2015)^[16] in conjunction with Red Media Technology at Bridford Barytes mine, Bridford. The 221 trial period was a duration of 3 months to assess the performance of the pellets on a realistic timescale. 222 The experiment consisted of a 1m³ tank containing compressed pellets (CP); mine water was 223 delivered to the tank and samples were taken throughout the operation, including pH readings. 224 Minewater was delivered to the test rig using a peristaltic pump with flexible pipework from the adit 225 discharge point. The flow rate into the test rig was initially set at approximately 15% of the mine 226 discharge flow and was adjusted to ensure consistent flow through the media tank (110 l/hr). Initial 227 residence time of one hour was altered as the trial continued so as to give data for additional hourly 228 intervals up to 8 hours residence time. Metal concentrations were determined by ICP-MS as described 229 above. Samples were collected from the inlet and output from the tank, filtered and preserved as for 230 the laboratory studies.

Analyte concentration data collected from the laboratory tests and field scale trial have been used to calculate the metal removal efficiency of each pellet form, as well as the adsorption capacity and pH neutralising capability; the results will allow an evaluation of which pellet is most suitable for reducing the Zn load from Bridford to the river Teign.

235 2.3. Alternative Treatment Method using Biochar

236 Biochar is a black, carbon rich solid produced by thermal decomposition of biomass, similarly 237 to charcoal. Typically, it has a wide range of characteristics which depend upon the feedstock used; 238 this affects the chemical and physical properties of the biochar and consequently how it acts as an 239 adsorbent. The test data described here [21], quantified the sorption capabilities of pelletized biochar 240 supplied by the United Kingdom Biochar Research Centre (UKBRC). Varying forms of feedstock 241 were tested at different pyrolysis temperatures (550°C and 700°C) including char produced from 242 forestry waste, municipal waste, and agricultural waste. Following a similar methodology to the 243 experiments for the red media study, adsorption rates and adsorption capacities were determined for 244 the same mine adit water. Metal concentrations were analysed by ICP-MS and ICP-OES as described 245 above.

246 2.4. *River Teign Metal Concentrations*

247 The Environment Agency (EA) act as the competent authority to implement the requirements 248 set out by the WFD and closely monitor the quality of water courses within England. Data provided 249 by the EA's water quality archive has been extracted to determine the mean concentrations of the 250 river Teign for dissolved Zn from 2000 to 2020. Analysing total dissolved metal concentrations forms 251 the first stage of a tiered approach to assessing the classification of a water body in the UK ^[10], if the 252 Teign exceeds the standard EQS value of 13.8, then it will progress to the next tier. Bioavailability 253 data is accessible after 2015 from EA monitoring data, identification of the bioavailable concentration 254 of the metal allows direct comparison with the bioavailable EQS (10.9 μ g/l for zinc) and forms the 255 second tier for assessing compliance of the Teign with the WFD.

256 Several sample locations along the course of the river Teign have been selected to represent 257 changing dissolved metal concentrations downstream from Bridford mine (ESI, S3). Closest to the 258 mine adit is the Rookery brook tributary which flows into the Teign. Further downstream east of 259 Canonteign is the Beadon brook past Wheal Exmouth mine site. Discharges sourced from Bridford 260 mine and Wheal Exmouth are intercepted by the Teign at Chudleigh Bridge. Dissolved 261 concentrations of Zn, Cd and Pb were obtained for these selected sites from the EA, as well as some 262 bioavailable data for Zn, calculated using the physiochemical parameters DOC (Dissolved Organic 263 Carbon), pH and Ca/Hardness (ESI, S8). Notably, concentrations of Cd and Pb were frequently below 264 the limit of detection (LOD), particularly from 2000-2010, these results therefore have a high 265 uncertainty.

266

267 2.5. Real-World Application Model

268 Using mean bioavailable metal concentration data and flow data from Chudleigh river gauging station available from the National River Flow Archive, the average load of Zn, Cd and Pb into and 269 270 within the river Teign at Chudleigh has been calculated using a simple spreadsheet model ^[14] (ESI, 271 S10), which simply combined flows and concentrations from the mine adit, with river data (flow and 272 concentrations) in order to generate loads of the trace metals entering the river and therefore the mine 273 adits contribution. River metal concentrations were available online from the Environment Agency's 274 Water Information System. Combining the EQS for the metal within the river with the flow, provided 275 a 'target' metal load to be achieved. The actual load was calculated by multiplying the latest 276 monitoring concentration data by the flow. Subtracting the 'target' metal load for EQS compliance 277 from the current load generated a load of metal required to be removed from the adit flow. It was 278 then a simple case of using the pellet metal adsorption capacities to estimate the amount of pellets 279 per year (tonnes) required to reach the EQS for the water quality monitoring point at Chudleigh. 280

281 3. Results

282 3.1. Removal Efficiency Results

Zn concentration data at Bridford mine adit is presented in figure 3. The results show Znconcentrations over a 24-hour period influenced by the different pellet forms.

285 The PP show a steady decline in Zn concentration within the first 2 hours from 11600µg/l to 286 8900µg/l, at 24 hours the final concentration is 616µg/l. The FAE pellets show a similar trend in the 287 first 2 hours with concentrations falling from 11300µg/l to 8410µg/l, at 24 hours Zn concentration is 288 311µg/l. The CP exhibit the steepest decline in Zn concentration and hence the fastest removal rate 289 with concentrations decreasing from 9643µg/l to 575µg/l in just 2 hours. Concentrations fall to 43.8µg/l 290 at 24 hours. Finally, the FP show the slowest decrease in Zn concentrations within the first 2 hours 291 $(9643 - 1388 \mu g/l)$. However, afterwards, concentrations rapidly decline to $68.9 \mu g/l$ at 24 hours. These 292 results reveal that the adsorption efficiency is strongly influenced by the pre-treatment of the pellets.

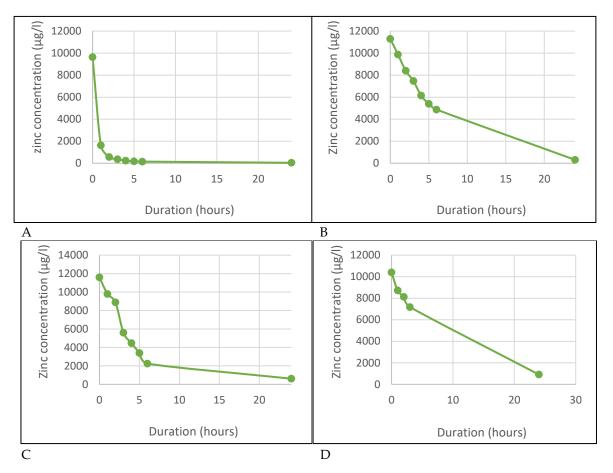


Figure 3. Zinc concentrations over a 24-hour period influenced by the different pellets.
A=Compressed pellets (CP), B=Fired acid-etched pellets (FAE), C=Powdered pellets (PP), D=Fired pellets (FP).

Levels of pH of the mine water during the experiments show that all the pellets have neutralising capabilities and produce alkaline conditions (Table 1). The CP and FP have a greater pH increase compared with the other pellets, particularly the FP which have the largest pH increase of 4.68. A limitation of the pH test is that data for the FAE and PP pellets was recorded at a shorter duration of 6 and 24 hours respectively.

Table 1. pH changes of the mine adit water using the different types of pellet. Raw data extracted
 from Turner (2017) ^[13] and Hill (2016) ^[14].

	pH of mine adit water			
Duration	Compressed pellets (CP)	Fired pellets (FP)	Fired acid-etched pellets (FAE)	Powdered pellets (PP)
Start of experiment (0 hour)	4.65	4.65	3.78	4.59
End of experiment	7.80 (53 hours)	9.33 (53 hours)	5.5 (6 hours)	8.84 (24 hours)

³⁰³

The removal efficiencies for Zn have been calculated using starting and final Zn concentrations and are summarised in table 2 (ESI, S4). The results show the CP to have the fastest rate of removal for Zn within the first 2 hours, achieving a high removal efficiency at 53 hours. The FP achieve the highest removal efficiency at 53 hours despite the slowest decrease in Zn concentrations at the

- 308 beginning of the experiment. The PP and FAE pellets show slightly lower removal efficiencies than
- the other pellets at 24 hours, but still reach a removal efficiency of 95%+.

310

Hours	Removal Efficiency for zinc (%)			
	Compressed	Fired	FAE	Powdered
2	73.7	22.0	25.6	23.3
24	99.5	99.3	97.2	94.7
53	99.8	99.9	-	-

311 Table 2. Efficiency of the different pellets for adsorbing Zn at 2, 24 and 53 hours [13,14].

312

Results from the adsorption capacity column experiment are shown in Table 3. Limited experiment duration meant that the highest capacity achieved was calculated using the starting and final concentration of the analytes, the weight of the pellets (CP 589g), (FP=410g), and the amount of liquid flowing through (1ml/min)^[14]. Due to the adsorption capacity not being sufficiently reached in this experiment, more realistic capacities for the CP were used from the field scale trial by Comber (2015)

318 for the Real-world application model.

Table 3. Highest adsorption capacities achieved from the column experiment for the CP and FP^[14].

320

Highest adsorption capacity		apacity	Adsorption capacity of pellets (mg/kg)		
reached			Zn	Cd	Pb
Compresse	ed Pellet		>105.6	>1.1	>5.36
Fired Pelle	t		>150	>1.56	>3.89
Field scale	trial (Compressed	l pellet)	8743	35.40	2089

321

322 The high removal efficiency of the CP is supported by the field scale trial conducted by Comber 323 (2015) ^[16]. Figure 4 shows the removal efficiency of the pellets over a 3-month period. Influent 324 concentrations of metal were relatively stable varying by only up to 11% (relative standard deviation) 325 for the different metals. The results reveal >80% of the Zn is removed within the first 10 days of the 326 experiment. After this period, the removal efficiency gradually falls until it remains at below 40% 327 after 40 days. Cd and Pb follow a similar trend but with a marked increase in removal after 70 days. 328 These results suggest that the RM pellets require at least 2 hours to be efficient and achieve >70% 329 removal, uptake is reduced greatly up to 24 hours and beyond (ESI, S5).

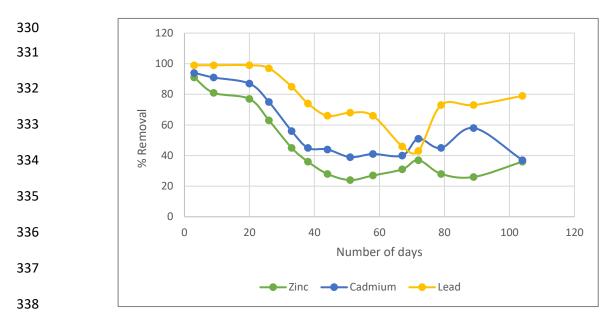
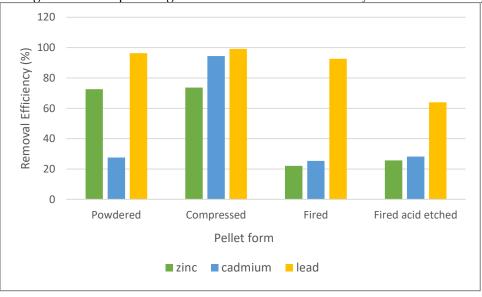
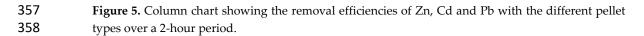


Figure 4. Graph showing results from the field scale trial. Removal efficiency of the compressed
 pellets for adsorbing filtered zinc, cadmium and lead over a three-month period at Bridford Barytes
 mine. Data taken from Comber (2015) ^[16].

When compared with the priority substances Cd and Pb (Figure 5), Zn appears to have the most similar adsorption rate to Cd, which is highest when influenced by the CP and lowest with the FP and FAE pellets. The results show Pb to have the greatest removal compared to Cd and Zn with all the pellets, especially the CP which exhibit nearly 100% removal efficiency. Notably, the data only shows results for a 2-hour duration; the FP are recognized to have the slowest removal efficiency during this time despite the greatest overall removal efficiency as demonstrated by figure 3 ^[13].



356



The results for the different biochar feedstock are shown in figure 6 at pyrolysis temperatures of 550°C and 700°C (ESI, S6). Overall, the feedstock with the highest removal efficiency after 2 hours is the agricultural waste (Miscanthus straw pellet, wheat straw pellet and oil seed rape) with analyte removal of over 80%. Forestry waste and municipal waste have the lowest removal efficiency compared to the other types of feedstock. Pb is the most effectively removed analyte with a removal rate of >90% for the agricultural waste, whereas Zn has the lowest removal efficiency for all the biochar feedstock. Notably, there is no real difference between the removal efficiency at pyrolysis temperatures of 550°C and 700°C, except lead has a slightly higher removal efficiency at a temperature of 700°C.



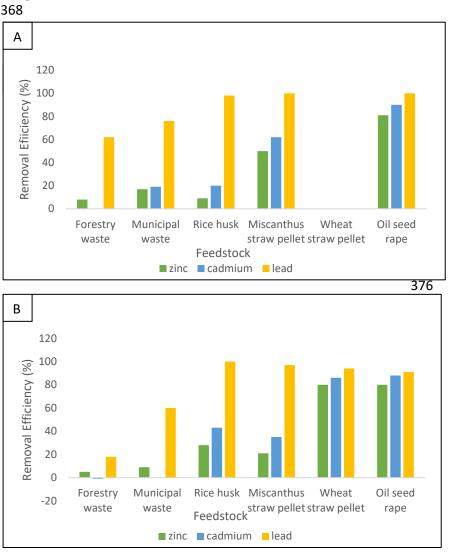


Figure 6. Column charts showing the removal efficiency of biochar at pyrolysis temperatures of 550°C
 (A) and 700°C (B) for Zn, Cd and Pb ^[21].

386 *3.2. River Teign Metal Concentration Results*

387 Selected sample locations downstream of Bridford mine are presented in figure 1 with average 388 dissolved Zn concentrations at each locality calculated from 2000-2020. Estimates of Zn concentrations at the adit have been made: 11,170µg/l^[22], 8,911µg/l^[14], 11, 200µg/l^[13] and 11,400µg/l 389 390 ^[16]. These values show that the adit acts as a point source of consistently high Zn values of around 391 11,000µg/l. Downstream of the adit, mine waters enter the Rookery brook where average Zn 392 concentrations are 471.8µg/l, this is considerably higher than upstream values of 49µg/l documented 393 by Hill (2016)^[14], owing to the mine discharge from Bridford. Further downstream, Zn concentrations 394 are reduced to 205.5µg/l at Beadon brook and then to 32.7µg/l at Chudleigh bridge. Whilst Zn levels

are observed to decline downstream, they remain above the EQS of 13.8µg/l throughout the courseof the Teign before entering the lower estuary where levels are reduced to 4.8µg/l.

397 Dissolved concentrations of Zn, Cd and Pb recorded at the sample locations have been collated 398 to show the changing metal concentrations between 2000 and 2020 (ESI, S7); the results are presented 399 in Figure 7. The Rookery brook PTCW (Prior to Confluence With river Teign) data shows Zn levels 400 to initially be declining followed by a slight upward trend after 2013. Concentrations still greatly 401 exceed the EQS with levels of 407µg/l in 2016, almost 30 times the EQS. Cd and Pb show a similar 402 trend of levels greatly exceeding the EQS despite an overall decline in recent years. Downstream at 403 Beadon brook, Zn concentrations fluctuate yet show a general decline to 138.9µg/l in 2018; this is still 404 10 times above the EQS. Cd levels are comparable to Zn with declining concentrations of 1.64µg/l in 405 2018, 20 times above the Cd EQS of 0.08µg/l. Meanwhile, Pb levels remain consistently below the EQS 406 of 7.2µg/l, with levels recorded at 1.71µg/l in 2019. Further along the river Teign at Chudleigh bridge, 407 metal concentrations are significantly lower than the previous localities. However, dissolved Zn 408 remains above the EQS and shows rising levels since 2014 to 42µg/l in 2019; this is still 3 times the 409 EQS. Cd follows a similar trend but appears to be steadily declining in recent years to $0.19\mu g/l$, 2

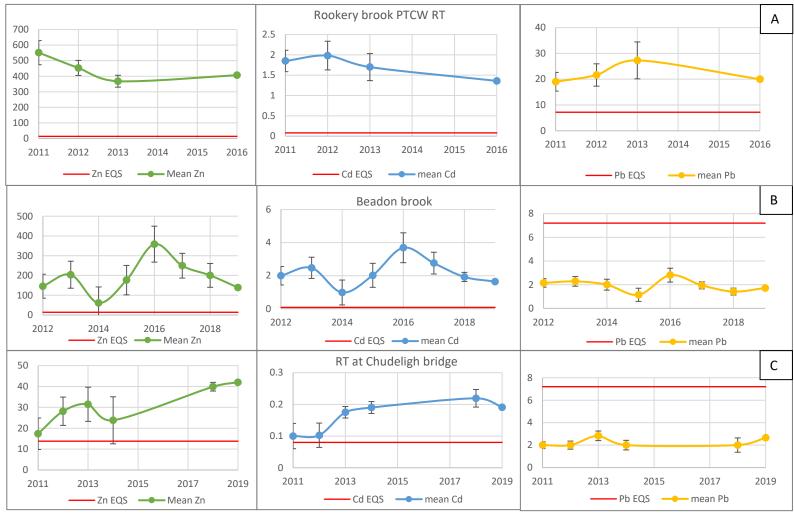


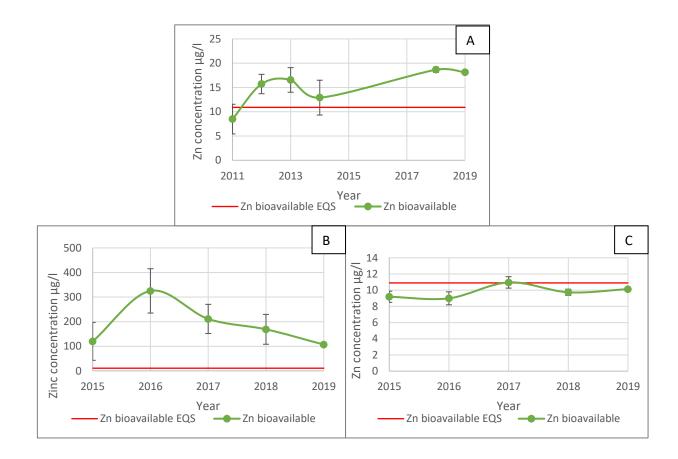
Figure 7. Dissolved metal concentrations (μg/l) compared with specific EQS along sample points of the river
Teign. Row A shows concentrations of Zn, Cd and Pb at Rookery brook from 2011 to 2016. Row B shows metal
concentrations downstream at Beadon brook from 2012 to 2019. Row C shows concentrations from Chudleigh
bridge from 2011 to 2019. Data collected from the Environment Agency water quality archive.

- 415 times the EQS. Pb levels, however, continue to stay below the EQS at $2.65\mu g/l$.
- 416 Identifying the bioavailable fraction forms the 2nd tier of assessing the risks posed by a
- 417 pollutant. Concentrations of bioavailable Zn for 3 sample locations have been calculated with the

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Biomet tool using DOC, pH and hardness data provided from the EA open data (ESI, S8). DOC
ranged between 2.8 and 4.7mg/l, pH ranged from 7.24 to 7.41 and hardness ranged from 24.2 to
37.3mg/l. Together, these results show that the bioavailable Zn fraction exceeds the EQS at both
Chudleigh bridge (18.1µg/l) and Beadon brook (107µg/l) (Figure 8). For the river Teign at Preston,
bioavailable Zn has stayed closely below the EQS (10.13µg/l).

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- 424



425

Figure 8. Annual mean bioavailable Zn levels for the river Teign at Chudleigh bridge (A), Beadon
Brook (B) and Preston (C), compared to the bioavailable EQS for Zn. Data calculated from EA water
quality archive ^[8].

429 *3.3. Real-World Application Model*

430 The mean bioavailable concentration of Zn at Chudleigh Bridge was $18.1\mu g/l$ in 2019. This was 431 combined with flow data at Chudleigh (5.32m³/s) to estimate the annual load from Bridford 432 downstream to the river Teign; the load was calculated to be 1210kg/yr. As well as this, the capacity 433 of the pellets was retrieved from adsorption capacity experiments (ESI, S9). The duration of the 434 experiment for the CP and FP were limited, therefore maximum adsorption capacities were not 435 reached, however the highest capacities achieved were recorded (Table 3)^[14]. For the model, capacities 436 from the field scale trial were used for a more representative result; the CP were found to have a 437 capacity of 8743mg/kg for Zn, and 35.40mg/kg for Cd. The most efficient biochar from the experiment 438 was agricultural biochar, with a capacity of 11000mg/kg [23]. Compared to the capacity of the wood 439 biochar which has been observed at 395.8mg/kg^[24]. The results from the model are shown in table 4; 440 estimates of the costs of the pellets have been calculated on the basis that 1 tonne of pellets costs 441 £88.95 to dispose of at landfill [13].

442 443

Table 4. Table showing the amount of pellets/biochar feedstock required in tonnes/yr to lower Zn levels to the fixed EQS at Chudleigh, based on EA metal concentrations in 2019.

Treatment Method	Tonnes/yr required (assuming 100% efficiency)	Tonnes/yr required based on removal efficiencies from this study	Cost
Compressed pellet (CP)	138	383 (36% efficiency after 3 months)	£34,067 a year
Fired pellet (FP)	8064	8064 (99.9% efficiency after 53 hours)	£717,292 a year
Agricultural biochar	110	137.5 (80% efficiency after 2 hours)	£12,230
Wood biochar	3056	15,280 (20% efficiency after 2 hours)	£1,359,156

444

445 The results from the model reveal that the agricultural biochar costs the least amount to reduce 446 Zn levels in the Teign. However, the removal efficiency was only tested up to 2 hours, therefore this 447 is not a realistic value as the removal efficiency is expected to drop over time. The CP would have a 448 more realistic application as the field scale trial showed the removal efficiency to drop to 36% after 3 449 months in the water; despite this drop, only 383 tonnes of pellets a year would be needed to reduce 450 the Zn levels, costing £34,067. The lower capacity of the FP and lack of removal efficiency data over 451 a longer duration makes it an infeasible treatment method costing £717,292 to dispose of at landfill. 452 The wood biochar has the lowest removal efficiency and would require 15,280 tonnes a year, again 453 an infeasible method. Using the CP, reducing Cd levels below the EQS would require 898 tonnes/yr 454 of pellets, amounting to £79,877; this would cost more than 2 times the cost of reducing Zn levels. 455 Dissolved Pb concentrations were below the EQS and therefore not considered in the model.

456

457 4. Discussion

458 4.1. Pellet Removal Efficiency

459 The data from this study suggests the most suited pellet for removing Zn loads from Bridford 460 are the CP. Fast adsorption rates allow >70% of the metal to be absorbed within the first 2 hours of 461 experimentation. This efficiency is supported by the field-scale trial, with rapid adsorption of Zn 462 within the first 20 days (>80%). At the end of the 3-month trial, the removal efficiency drops to <40%, 463 suggesting that the capacity of the pellets had not been exhausted. It was assumed that precipitation 464 of metals as insoluble hydroxides owing to the alkaline pH of the RM pellets or co-precipitation with 465 iron and aluminum oxy-hydroxide floccs, becomes the dominant process blocking sorption sites and 466 consequently lowering the adsorption efficiency ^[22]. The higher removal efficiency of the CP can be 467 attributed to its higher surface area of 27.9m²/g compared with other pellets (35 times greater than 468 the FP) [14]. Notably, the FP have a slower initial removal efficiency, yet remove 99.9% of Zn at 53 469 hours. Both pellets cause an immediate pH increase when added to solution, although the FP result 470 in the highest pH increase of 4.68, enabling the formation of precipitates such as iron hydroxide to 471 further drive metal removal. Whilst the adsorption kinetics experiments have identified the CP and 472 FP as having the greatest removal efficiency, the faster removal rate of the CP means a lower phase-473 contact time is needed between the pellets and water; this makes it more suited to a real-world 474 application. Pb is observed to adsorb more strongly than Zn and Cd, this is possibly due to its greater 475 partition coefficient [25].

The results from the experiment are supported by other studies using RM pellets ^[26]. Crushedpellets with a greater surface area (like the CP) have been found to be most efficient, with enhanced

478 metal adsorption taking place at an optimum pH of 5/6 for Zn. Significant uptake of Zn has been 479 documented within the first few hours of experimentation, with a less pronounced uptake after 24 480 hours ^[27], in line with the results from this study. Interestingly, the FAE pellets had a lower removal 481 efficiency compared to the CP and PP; however other studies have proved acid treatment to be highly 482 effective in aiding adsorption [18]. Although surface area is likely to be a key driver in terms of sorption 483 capacity owing to increased sites being available for metal exchange, the charge on the metals of 484 interests as well the adsorbent media themselves will also influence the ability to bind metals. The 485 pH value of the solution in which the pellets are in greatly effects the adsorption and desorption of 486 metal ions. At a low pH the charge on the outside of the red mud has a high positive charge density, 487 meaning a low uptake of metal ions due to electrostatic repulsion but a high adsorption of anions. 488 However, when the pH increases the negative charge density on the surface increases, increasing 489 metal adsorption and lowering non-metal adsorption. The presence of Al(OH)₃ (gibbsite) and 490 FeO(OH) (goethite) which are hydroxylated surfaces helps to absorb H+ ions^[18] for red media but will 491 have little impact for biochars which exhibit much less variable and more neutral pH.

492 4.2. Biochar Removal Efficiency

493 Previous studies have demonstrated the remediation potential of Biochar, particularly as a soil 494 modification where application has been seen to reduce bioavailability of toxic metals and 495 simultaneously promote plant growth. Maximum removal efficiencies (>95%) have been observed at 496 high pyrolysis temperatures (650°C) which greatly influence the success of the treatment method ^[28]. 497 Other parameters such as contact time, particle size and the type of biochar feedstock used have also 498 been considered as important factors.

499 Results from this study have shown the type of feedstock to be an important influence on the 500 removal efficiency of Zn, Cd and Pb, rather than pyrolysis temperature. Forestry feedstock had the 501 lowest removal efficiency whilst agricultural waste had the overall highest. This can be explained by 502 the pyrolysis temperature at which the biochar is produced at. Higher temperatures produce a higher 503 ash content which raises the pH and consequently aids metal adsorption, with maximum adsorption 504 recorded at pH 5^[29], similarly to the RM pellets. This ash component is accountable for significant Pb 505 immobilisation, explaining why Pb had the greatest adsorption rate in the experiment. Forestry waste 506 has a low ash content and hence low adsorption rates. Other studies support this concept where lower 507 pH (7.9) has been observed in wood biochars, compared to other feedstock which significantly 508 increases the pH to 9 and above [24].

509 4.3. River Teign Compliance

510 High metal concentrations do not automatically mean that a water body is failing, 511 disproportionate results could lead to unnecessary investment in treatment methods to reduce metal 512 concentrations when the toxicity is overestimated. However, dissolved Zn concentrations exceed 513 standards at all sample locations downstream of Bridford mine, suggesting it to be a significant 514 source of Zn to the river Teign. Bioavailable data shows that Zn is present in its most ecotoxic form, 515 exceeding the bioavailable EQS all the way downstream to Preston, over 10km from Bridford mine. 516 Bioavailability data therefore helps identify hotspots of high Zn levels such as Beadon Brook and 517 Chudleigh where levels are of environmental concern; the metal is available for biological uptake and 518 present at a concentration that may be harmful to plants and animals. Physiochemical parameters 519 that control the bioavailability of a metal include DOC, pH and hardness. Optimal conditions for 520 bioavailable Zn consist of a DOC ranging between 2.48 and 22.9mg/l and a pH between 5.7 and 8.4 521 ^[30]; results from this study reveal conditions from the Teign at Chudleigh to have a pH of 7.24-7.41, 522 and a DOC ranging between 2.8 and 4.7mg/l.

523 Despite this, assessing the compliance of a water body is complex with many factors to consider.
524 South Devon has naturally high occurring concentrations of heavy metals including Zn owing to its
525 metalliferous background geology. Existing high Zn levels may result in the development of tolerant

species that can hyperaccumulate metals ^[31]. Therefore, the effects of Zn may not be as damaging to
 ecosystems as studies suggest.

528 Cd levels in the Teign also exceed the EQS and are rising at some of the sample locations. 529 Independently, the impacts of Cd and resulting effects on ecosystems are beyond the scope of this 530 project. However, the synergistic effects of metals such as Zn, Cd and Pb together have been 531 documented and observed to increase fish mortality ^[5]. It is therefore important to investigate the 532 effects of combinations of metals to assess the threats posed to the environment.

533 4.4. Application to Bridford Mine

534 Mine adit drainage tends to be discharged from a single point as it was the main mechanism of 535 removing water from mines to prevent flooding. In terms of remediation, it is therefore relatively 536 straightforward to divert the flow of mine adit discharges through beds of adsorbent material for 537 passive treatment processes, often using gravity to feed to avoid unnecessary pumping and the 538 requirement of power to the site. The practicalities for application of this treatment at the case study 539 site (and likely elsewhere) is considered straightforward. According to the real-world application 540 model, the CP and agricultural biochar are the most promising treatment methods for adsorbing Zn 541 at Bridford mine. The removal efficiency of the RM pellets is a result of pre-treatment which affects 542 the porosity, surface area and adsorption capacity of the pellets. The CP have the highest adsorption 543 capacity due to their larger surface area and would ultimately require less production and lower 544 disposal costs. The FP have a much lower adsorption capacity, resulting in the need for 58 times more 545 tonnes of pellets a year compared to the CP. Hill (2016) [14] and Turner (2017) [13] similarly found that 546 you would need 44 times more FP than CP to efficiently remove Zn at the mine site. However, despite 547 the slower adsorption rate of the FP, its ability to significantly raise pH may prove useful for 548 increasing precipitation reactions and consequently removing metals via the formation of 549 hydroxides. A limitation of this study is the difficulty in comparing the mass of pellets required for 550 metal removal when removal efficiency has been measured over different time frames. However, it 551 provides an insight into the potential for the CP and FP to act as an efficient low-cost adsorbent for 552 UK mine sites. The PP also have potential for effectively removing metals at Bridford, however 553 adsorption capacity data and a field scale trial would be necessary.

Despite the success of the CP, the field scale trial by Comber (2015) ^[16] highlighted a few issues that may affect the pellets ability to act as an adsorbent. Firstly, the pellets lacked rigidity, resulting in a loss of structural integrity during the trial; this is problematic for a realistic application of the treatment method. Also, the precipitation of ochre (iron hydroxide) resulted in a build-up of iron on the pellet surface, blocking adsorption sites. Although, it also leads to an increase in co-precipitation of other metals, thus limiting the mobility of dissolved metals in the mine water ^[32].

Field scale trials of biochar treatment have shown that the effectiveness decreases over time (biochar ageing effect) ^[33]. However, unlike the CP, biochar is persistent in the environment and its application may be prolonged. This is particularly the case with high temperature biochars which have a greater carbon stability ^[34], making it a more effective adsorbent. Biochar therefore offers an attractive remediation alternative to the RM pellets. Although, the effects of potentially hazardous substances in biochars because of the feedstock used and the pyrolysis process are still largely unknown ^[35].

567 Each year, 90 million tonnes of RM are produced globally, making it widely available as an 568 adsorbent [18]. RM as a raw material although rich in aluminium and iron, does not pose a particular 569 threat to the environment as it binds other metals which might be present as impurities very strongly. 570 Pre-testing of the leaching of metals from the pellets (unpublished data) should have very little 571 desorption into deionised water. Biochars also tend to be relatively inert as organic contaminants are 572 destroyed via the charring process and any residual metal levels are likely to be only very minor 573 impurities. However, once potentially toxic metals have been adsorbed to the media it is viewed as 574 a hazardous material and has to be disposed of accordingly. Although it may be used within the 575 mine site for land remediation, and off-site disposal is costly, valued at £88.95 per tonne (as at April

576 2018) [13]. Currently, the pellets can be disposed of in mine tailings in agreement with the EA, however, 577 where this is not possible, they are sent to an inert landfill. One viable solution to reduce disposal 578 costs would be to drain the pellets after use to achieve a greater % of dry weight ^[14]. Also, to further 579 increase the efficiency of the pellets, a cell-based system could be used where pellets are placed 580 successively next to each other. This design would ensure that pellet capacity is not all exhausted at 581 once, prolonging their effect of metal removal. Ultimately recovery of metals from the media and 582 recycling the metal would be the most sustainable option, within a circular economy, but the 583 wholesale value of the trace elements recovered would need to be higher than current market prices 584 for this to be viable. Costs for fabrication of any remediation adsorbent beds, pumping requirements 585 and media purchase were beyond the scope of this study and would also be dependent on the scale 586 of operation, market prices at any given time and pumping requirements.

587

Adsorption is an economical remediation technique, owing to the abundance of waste materials, their low cost, and high capacities. It is a much more practical option for mine sites than the current most widely used treatment method activated carbon (AC). AC is inaccessible for most remediation projects due to its high cost, which is typically more than 1000 Euros/tonne, equivalent to £914.281/tonne ^[36]. The metal-removing capabilities shown by the RM pellets and biochar are therefore more suited to application at Bridford mine than limited methods like activated carbon.

594 Realistically, for the river Teign to comply with water quality standards, other inputs need to be 595 addressed. Whilst Bridford mine is a significant source of Zn, it cannot solely be accounted for the 596 failure of Zn levels downstream in the Teign. Other mine inputs like Wheal Exmouth near 597 Canonteign are a potentially major source of Zn as shown by the high concentrations at Beadon brook 598 downstream of the mine site. During the peak of mine operation (between 1851 and 1874), outputs of 599 Pb and Zn are estimated to be 11,759 tonnes and 1589 tonnes respectively ^[2]. Treatment of mine water 600 at Wheal Exmouth is necessary to reduce metal concentrations below the EQS, particularly in the case 601 of Cd which would require 898 tonnes of pellets a year applied at Bridford alone to reduce levels 602 below the EQS. Moreover, mine adits only represent point sources of pollution, diffuse sources such 603 as runoff from tailings and road surfaces should also be investigated for their contribution to Zn, Cd 604 and Pb levels.

605 5. Conclusions

This study has highlighted the long-term impact of historical mining on our local water
resources, demonstrating the need for protection and assurance of water quality, implemented by
key legislation like the WFD.

609 The consistent exceedance of Zn and Cd environmental quality standards in the river Teign has 610 formed the rationale for evaluating potential treatment methods. Adsorption techniques for mine 611 remediation are topical due to their low cost and abundance; this study has proven the potential for 612 pelletized RM and biochar as effective adsorbents. Pellets with a greater surface area and higher 613 adsorption capacity such as the CP demonstrate high removal efficiencies for Zn, Cd and Pb within 614 the first 2 hours (73.7%, 94.4% and 99.2% respectively). Agricultural biochar formed at high pyrolysis 615 temperatures has also been observed as a promising material for removing ecotoxic metals (>80% 616 removal within the first 2 hours). Limited data on the FAE pellets and PP meant that their application 617 to a mine site could not be determined, however, they do exhibit neutralizing capabilities as well as 618 effective adsorption. 619 Treatment methods need to follow the principle of sustainable development by improving the

619 Freatment methods need to follow the principle of sustainable development by improving the 620 status of a water body whilst considering the costs and benefits of their application. Reusing the 621 hazardous RM as an adsorptive material supports this concept of sustainability, especially the CP 622 which can be disposed of at only £34,067; this is much more economically viable than other treatment 623 the bill of th

- 623 methods like activated carbon.
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