Preparation and Optimization of Pyrophosphate Bath for Copper Electroplating of Microwave Components

L.G. Bhatgadde and S. Mahapatra Indian Institute of Technology, Bombay-400 076

ABSTRACT

The principles of copper deposition from pyrophosphate electrolytes have been explained. Based on these principles, a method of preparation of plating bath from basic constituents has been described. It was found that copper pyrophosphate is precipitated from solutions of copper sulphate and potassium pyrophosphate at a pH of 5.0. For maximum efficiency, copper pyrophosphate has to be dissolved in potassium pyrophosphate in a weight ratio of 1 : 4 or a total P_2O_7 : Cu ratio of 7.5 : 1. By using optimum values of anode : cathode area, 2.5, pH, 5.0, temperature, 55°C and a cathode current density of 0.8 A/dm², bright, adherent copper electroplates were deposited on electroless copper plated Al_2O_3 substrates employed in microwave components.

1. INTRODUCTION

Copper plating is required on hybrid microwave integrated circuit components for providing a highly conducting layer on ceramics and plastics substrates. These substrates are previously plated with thin metallic films by vacuum methods or electroless techniques. The electrodeposited coating must adhere well to the underlying substrate.

The conventional copper plating baths consist of copper sulphate-sulphuric acid (pH: 0.3-2.0) or copper cyanide-sodium cyanide (pH: 12.0). The acid fluoborate baths (pH: 0.2) are used less frequently. These acidic baths are highly corrosive for plating of delicate IC components, while the alkaline cyanide baths pose the problems

of environmental disposal. The need for a non-corrosive and non-toxic electro-plating bath thus becomes inevitable.

The weakly alkaline pyrophosphate bath (pH: 8-9) provides an attractive choice. The bath is known to produce bright, fine grained, smooth deposits of low internal stresses, has a high throwing power and is already popular for plating through holes of the *PCBs*². Unfortunately the indigenous sources of this bath are irregular. This situation has forced many platers to import these formulations. The purpose of the present investigation is to understand the principles of copper deposition from pyrophosphate electrolytes and thereby optimize the quantities of bath ingredients to enable it to be prepared from the indegenously available constitutents.

2. PRINCIPLES

Coppet forms complex anions such as $CuP_2O_7^{2-}$, $Cu_2P_2O_7^{6-}$ and cations such as $Cu_2P_2O_7^{-}$ with pyrophosphate. However, the pH ranges of formation of these complex ions are not precisely known.

On adding a solution of potassium pyrophosphate, $K_4P_2O_7$ to a solution of copper sulphate, $CuSO_4$ 5 H_2O , a precipitate of copper pyrophosphate, $Cu_2P_2O_7$.3 H_2O is produced according to the reaction,

$$2CuSO_4 + K_4 P_2 O_7 \rightarrow Cu_2 P_2 O_7 + 2K_2 SO_4$$
(1)

The precipitated copper pyrophosphate can be dissolved in solutions containing different quantities of potassium pyrophosphate. By carrying out electrolysis of these solutions containing different weight ratios of P_2O_7 : Cu, the most optimum ratio giving a highly adherent copper deposit with maximum efficiency can be determined.

The complex prepared as above dissociates giving Cu^{++} and $P_2O_7^{+-}$ ions. On electrolysis using copper anodes, the main electrode reactions are,

$$Cu \rightarrow Cu^{++} + 2e^{-}$$
 anodic (2)

$$+ 2e^- \rightarrow Cu^0$$
 cathodic (3)

Besides, there are products of water decomposition arising from

$$\rightarrow H^{+} + OH^{-} \tag{4}$$

$$+ 2e^- \rightarrow H_2$$
 cathodic (5)

$$\rightarrow H_2O + \frac{1}{2}O_2 + 2e^- \qquad \text{anodic} \qquad (6)$$

The hydrogen gas formed causes cathode polarisation leading to a decrease in plating rate. To prevent this, NO_3 ions are added in form ammonium nitrate, NH_4NO_3 , which acts as

$$NO_3^- + 1OH^+ + 8\bar{e} \rightarrow NH_4^+ + 3H_2O \tag{7}$$

 NH_4^+ increases the anode corrosion and acts as a grain refiner for the deposits.

After long plating periods, pyrophosphate hydrolyses to orthophosphate as

$P_2 O_7^{4-} + H_2 O \rightarrow 2 H P O_4^{2-} \tag{8}$

This decreases the throwing power as well as ductility of the deposits. Orthophosphate also forms, if the bath is acidified below pH7 or is heated to >60°C. Its concentration should not exceed 100 g/l, in which case the bath has to be discarded.

Besides nitrates, iodides, bromides, oxalates, thiourea, dextrin, glycerol, formalin, citrates and sachharin have all been used as additives. However, the disadvantages of organic additives is the accumulation of degradation products in the bath necessitating their removal by continuous filtration.

3. EXPERIMENTAL

120 g of $CuSO_45H_2O$ (A.R) is dissolved in 700 ml distilled water contained in a one litre beaker. 200 ml of 100 g potassium pyrophosphate, $K_4P_2O_7$ was also prepared. The latter was added to former with continuous stirring. A precipitate of copper pyrophosphate formed. The addition was continued till the precipitation was complete, as evidenced by taking as alicot of the supernatant liquor and mixing it with $K_4P_2O_7$ solution to check for unreacted copper. The *pH* after complete precipitation was 5.0. Any excess of $K_4P_2O_7$ solution was avoided, as the same redissolved the precipitate. The volume of pyrophosphate solution thus consumed was 160 ml.

The precipitate was allowed to settle and the upper liquor containing K_2SO_4 was removed by decantation. It was washed by adding further quantities of distilled water. Washing was continued, till the copper liquor was free from SO_4 impurities. (Tested with dil $BaCl_2$ solution). Thereafter, it was filtered, dried at 110°C for 3 hrs. cooled and weighed.

A 300 ml of plating bath was made by dissolving 30 g of copper pyrophosphate prepared above, 85 g of $K_4P_2O_7$ and 4 g of $NH_4 NO_3$. This had a pH of 9.5, which was adjusted to 8.0 by adding pyrophosphoric acid, $H_4P_2O_7$. It was then filtered, taken in a 500 ml beaker and heated to 55°C on a thermostatically controlled hot plate-cum-magnetic stirrer.

The electroless copper plated Al_2O_3 substrates (2 × 1 inch, 25 mm thick) were electroplated. The plating jig consisted of two identical electrolytic grade copper anodes (2 × 2.5 inch, 5 mm thick), fitted vertically at a distance of 2.5 inch by screwing to a perspex plate (4 × 4 inch, 5 mm thick). The substrate was fixed in a copper rod holder and held in the middle of these two anodes. The plating was carried out at a constant current of 0.2 A for 2.5 hrs. The quantity of copper deposited was found out by weighing the substrate before and after plating.

The adhesivity of electroplated copper was qualitatively tested by using the conventional Scotch tape.

Likewise, five more baths each containing 30 g of copper pyrophosphate, 4 g of HNH_4NO_3 but different quantities of $K_4P_2O_7$ were prepared and the substrates were electroplated under identical conditions. These results are presented in Table 1.

Bath No.	$\begin{array}{c} Cu_2P_2O_7:\\ 3H_2O\\ (g) \end{array}$	K ₄ P ₂ O ₇ (g)	P ₂ O ₇ .Cu	C (Amp)	· V	Cu plated	d Adhesivity	Remarks
					(Volt)	(g)		
	30	85	5.54	0.2	0.2	0.086	poor	non-uniform deposit, anodes black
	30	105	6.52	0.2	0.2	0.217	excellent	bright uniform deposit, anodes pink
3.	30	125	7.50	0.2	0.2 for 0.5 hr 0.3 for 2 hrs	0.215	excellent	bright uniform deposit, anodes bright
4.	30	145	8.47	0.2	0.3 for 1 hr 0.2 for 1.5 hrs	0.219	good	- do-
	30	165	8.45	0,2	0.4 for 0.5 hr 0.3 for 2 hrs	0.250	poor	-do-
	30	185	10.42	0.2	0.5 for 0.25 hr 0.4 for 2.25 hrs	0.239	poor	-do-

Table 1. Effect of P_2O_7 : Cu ratio on performance of copper pyrophosphate electroplating baths

4. RESULTS AND DISCUSSION

The quantity of $K_4P_2O_7$ required for complete precipitation was 80 g and the weight of $Cu_2P_2O_7$. $3H_2O$ produced was 82 g. If reaction (1) is valid, the expected yield of $Cu_2P_2O_7.3H_2O$ should be 85 g. However, the difference of 3 g might be attributed to the losses during washings. As mentioned under section 3, this reaction is complete at pH: 5.0.

It will be evident from Table 1 that $Cu_2P_2O_7$ dissolves in $K_4P_2O_7$ for a weight ratio of P_2O_7 : Cu = 5.5. This value corresponds to the formation of a hexavalent anion viz, $Cu (P_2O_7)^{6-}$, which results from the dissociation of the complex produced as per the reaction,

$$Cu_{2}P_{2}O_{7} + 3K_{4}P_{2}O_{7} \to 2 [K_{6}Cu (P_{2}O_{7})_{2}]$$
(9)

It is also seen that the weight of copper deposited per unit quantity of electricity is minimum for the above bath No. 1. Besides, the anodes were black possibly due to formation of cupric oxides causing a decrease in anode efficiency. As the P_2O_7 : Cu ratio increased to 6.5 for bath 2, the quantity of copper deposited also increased more than two folds. Still, the anodes were plnk indicating the formation of cuprous oxide. However, for the ratio of 7.5 although the weight of copper decreased a little, the anodes corroded brightly. This occurs at nearly 100 per cent anode efficiency and renders the bath economical, since it does not become necessary to replenish the

expensive pyrophosphate salt. The adhesivity of copper electroplate was meeting the specification laid down for subsequent processing of the plated substrates.

5. CONCLUSIONS

- (i) Copper pyrophosphate can be produced by mixing a solution of copper sulphate with a solution of potassium pyrophosphate in a mole ratio of 1:1.
- (ii) Copper pyrophosphate can be dissolved in excess potassium pyrophosphate in a weight ratio of 1:4 or a $P_2O_7: Cu$ ratio of 7.5:1.
- (iii) By using a cathodic current density of 0.8 A/dm², temperature 55°C and pH, 8.0, highly adherent bright copper coatings have been obtained on electroless copper plated Al_2O_3 substrates.

ACKNOWLEDGEMENT

The authors are thankful to DRDO, Ministry of Defence, for their financial support.

REFERENCES

- 1 Lowenheim, F.A., Electroplating (McGraw Hill Book Co., New York), 1978, pp. 194–204.
- 2. Anthony, S. & Ramualdas, B., Metal Finishing Guide Book and Directory (Metals and Plastics Publications, Inc., N.J.), 1986, pp. 217-219.
- 3 Seliverstov, V.P., Izv. Vyssh. Uchebn. Zaved. Khim Teknol, 26 (1983), 883-884.
- 4 Minakawa, Todashi, et al., Japanese Patent, 78, 109, 826, 1978.
- 5 Loschkarev, M.A., et al., Vapr. Khim. Khim. Tekhnol, 56 (1979), 55-58.
- 6. Pilavov, Sh. G., & Egarova, A.L., Zashch. Met., 13 (1977), 734-73.
- 7. Raljewicz, Z. et al., Polish Patent, 120, 289, 1983.