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Electrospinning/Electrospraying coatings for metal microneedles: a design of experiments (DOE) and Quality by Design (QbD) approach

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1 **Electrospinning/Electrospraying coatings for metal microneedles: a design of**
2 **experiments (DOE) and Quality by Design (QbD) approach**

3

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25

26 **Abstract**

27 The research presented here shows QbD implementation for the optimisation of the key
28 process parameters in electrohydrodynamic atomisation (EHDA). Here, the
29 electrospayed nanoparticles and electrospun fibers consisting of a polymeric matrix
30 and dye. Eight formulations were assessed consisting of 5% w/v of polycaprolactone
31 (PCL) in dichloromethane (DCM) and 5% w/v polyvinylpyrrolidone (PVP) in ethanol.
32 A full factorial DOE was used to assess the various parameters (applied voltage,
33 deposition distance, flow rate). Further particle and fiber analysis using Scanning
34 Electron Microscopy (SEM), Differential Scanning Calorimetry (DSC),
35 Thermogravimetric Analysis (TGA), Fourier Transform Infrared Spectroscopy (FTIR),
36 particle/fiber size distribution. In addition to this *in vitro* release studies were carried
37 out using fluorescein and Rhodamine B as model dyes and *in vitro* permeation studies
38 were applied. The results show a significant difference in the morphology of resultant
39 structures as well as a more rapid release profile for the PVP particles and fibers in
40 comparison to the sustained release profiles found with PCL. *In vitro* drug release
41 studies showed 100% drug release after 7 days for PCL particles and showed 100%
42 drug release within 120 min for PVP particles. The release kinetics and the permeation
43 study showed that the MN successfully pierced the membrane and the electrospun MN
44 coating released a large amount of the loaded drug within 6 h. This study has
45 demonstrated the capability of these robust MNs to encapsulate a diverse range drugs
46 within a polymeric matrix giving rise to the potential of developed personalised medical
47 devices.

48

49 **Keywords:** Electrohydrodynamic atomisation, quality by design, transdermal delivery,
50 microneedles

51 1. Introduction

52 Quality by Design (QbD) involves taking a “systematic approach to development with
53 pre-defined objectives” focussing more on the product and processes based on science
54 and risk management [1,2]. A quality target product profile (QTPP) is established which
55 includes and defines all requirements that the final product is expected to meet and
56 satisfy (e.g. dosage form, strength, purity limits etc). Critical quality attributes (CQAs)
57 of a product and their potential interaction and impact during the manufacturing process
58 are also key [3] and are often associated with the design of the drug substance and the
59 manufacturing process. It is from identifying CQAs that a fitting limit/range is assigned
60 to each to make sure that the desired product quality is achieved. Critical process
61 parameters (CPPs) are factors which heavily impact the manufacturing process and
62 therefore need to be controlled and monitored throughout.

63 Electrohydrodynamic atomisation (EHDA) is a structure fabrication method that
64 utilises an electrical field to atomise liquids [4]. Branches of EHDA include;
65 electrospraying (ES; for particles), electrospinning (ESP; for fibers) [5,6] and
66 electrohydrodynamic bubbling (for bubble related structures) [7,8]. ES has evolved
67 from basic concepts [9,10] to being applied to polymers [7], ceramics [11], cosmetics
68 [12], antibiotics [13], insulin delivery [14], food industry [15], capsules [16,17],
69 anticancer drug delivery [18], brain drug delivery [19], buccal drug delivery [19], tissue
70 engineering [8], biomedical engineering application using hydroxyapatite [21,22,23,
71 24] and emerging drug delivery [25]. This engineering method has evolved to enable
72 development of new drug delivery devices such as contact lenses [26], patches [27] and
73 stents [28]. EHDA is a non-conventional solvent-based method, which, depending on
74 formulation properties, can be referred to as ES or ESP [29].

75 Several transdermal drug delivery strategies aim to enhance patient compliance when
76 compared to conventional routes [30] and also avoid first pass drug
77 hepatic/gastrointestinal metabolism [31]. The skins' formidable barrier, the stratum
78 corneum (SC, ca.10-20 μm thick), has proven challenging to overcome [32]. However,
79 transdermal microneedles (MNs) propose an appealing alternative to hypodermic
80 needles and oral medication with potential applications with chronic complications like
81 cancer, diabetes and Alzheimer's as well as monitoring systems for lithium levels as
82 EEG probes [33]. These devices are less invasive, more efficient and more patient
83 friendly [34]. They generally consist of arrays/patterns of individual solid needles
84 measuring 50-900 μm high and having a surface density around 2000 needles/ cm^2 ;
85 penetrating the SC in a painless manner [35,36]. Many therapeutic agents can be
86 delivered via the MN approach including macromolecules [37, 38], anticancer agents
87 [39] and other hydrophilic and hydrophobic compounds [40].

88 One of the earliest studies demonstrating EHDA as a viable technique to produce smart
89 MNs for drug delivery varied EHD process parameters to generate particles (100 nm to
90 3 μm) and fibers (400 nm to 1 μm) [41].

91 Both organic and inorganic composite MNs have shown capability of releasing API
92 following skin insertion [42]. FDA-approved synthetic biodegradable and water-
93 soluble polymers including poly-vinylpyrrolidone (PVP) and poly-caprolactone (PCL)
94 [43] have been identified as potential matrices for drugs and successfully exploited as
95 encapsulated agents. Reksamunadar et al demonstrated successful encapsulation of
96 α -carotene (1 wt. %) within a PVP (10 wt. %) matrix through ESP. These composite
97 nanofibers exerted the greatest antioxidant activity [44]. A study by Ronnander et al
98 showed that sumatriptan succinate encapsulated in PVP dissolving MNs (DMNs)
99 exhibited rapid drug release [36]. Whilst drugs encapsulated within a PVP matrix

100 demonstrate rapid release, drug loaded PCL MNs tend to show a more sustained release
101 profile. Anderson et al supports this as the *in vitro* release of PCL MNs loaded with
102 furosemide by diffusion was within 18 h at 37 °C [45].

103 This study focuses on the detailed evaluation of polymeric MN arrays coated using
104 EHDA. Polymeric formulations and the resultant particular and fibrous structures were
105 assessed. *In vitro* release, thermal, spectroscopic analysis, wettability (contact angle)
106 and diffusion studies to show dye distribution were performed. Mechanical and stability
107 assessments were also performed. In addition, release model fitting provided a valuable
108 insight into the potential release mechanism of dyes for the particular and fibrous
109 systems and permeation studies.

110

111 2. Materials and Methods

112 2.1. Materials

113 PVP (4.4×10^4 g/mol, 1.3 $\times 10^6$ g/mol) was obtained from Ashland,
114 UK, Polycaprolactone (PCL (1.4×10^4 , 8.0×10^4 g/mol), Ethanol, Dichloromethane,
115 Fluorescein and Rhodamine B (RhB) were supplied by Sigma Aldrich, Dorset, UK,
116 stainless steel microneedles (900 array) was purchased from Adminpatch (California,
117 USA) were all utilised in this study. All reagents were of analytical grade and were
118 purchased from Sigma Aldrich.

119

120 2.2. Methods

121 Implementation of QbD

122 Identification of quality target product profile and selection of critical quality
123 attributes

124 The protocol for QbD was applied in this study and examined for dye-loaded MN
125 coatings. In line with implementing QbD to the EHDA process a risk assessment was
126 carried out identifying the factors that can affect the process and the chosen critical
127 quality attributes (CQAs). The foundation of QbD is based on having knowledge to
128 exert control and better understanding of the relationship between CQAs and critical
129 process parameters (CPPs) which are essential for quality target product profile
130 (QTTP). There are many types of risk assessments that can be performed within a QbD
131 framework; examples of such assessments include; cause and effect (fishbone)
132 diagrams, preliminary hazard assessments (PHA) and failure mode and effects analysis
133 (FMEA). According to ICH Q8, QbD implementation begins with identifying the
134 quality target product profile (QTTP) which outlines the quality, safety and efficacy of
135 the product. The QTTP for the four dye-loaded formulations can be found in the
136 appendix. CQAs are defined as a physical, chemical, biological or microbiological
137 property or characteristic that should be within an acceptable limit, range, or
138 distribution to confer the desired product quality. Variability of CPPs has an impact on
139 the CQAs thus the management and control of them are essential. Preliminary studies
140 of solutions enable fixed concentrations being established for the solutions used in the
141 study. EHDA has two main process parameters: the flow rate and the driving force
142 (electric current/voltage). Here, the flow rate was the parameter being investigated.
143 Finally, the design space was identified; determining the optimal conditions.

144

145 **2.3. EHDA and DOE analysis**

146 Using JMP software, the DOE was created for each of the polymers (PVP and PCL) to
147 produce structures with desirable shape, size and polydispersity. This was achieved by
148 optimising the EHDA process i.e. altering various process parameters (voltage,

149 deposition distance and flow rate). A full factorial design was carried out which was
150 able to generate and verify the response surface plots. These plots encompass the
151 interactions between the formulation variables and process parameters to assure quality
152 in the product. Working within the limits of these in theory ensures quality. With a more
153 comprehensive design space/response surface plot, there is ample flexibility within the
154 process parameters.

155

156 **2.4. JMP Pro Software**

157 Prior to atomisation experiments, JMP software was used to generate the screening
158 design DOE. A full factorial design was then carried out and the responses and factors
159 were input into the system to optimise the system. JMP then analysed all results to
160 statistically explore the data and to visually illustrate the findings. The predictive
161 analytical tools (predictive profilers, response surface plot) which aid to build, enhance
162 and develop a model to predict what will happen with new processes or new risks.

163

164 **2.5. Solution preparation**

165 Solutions of 1 % w/v and 5% w/v low molecular weight (4.4×10^4 g/mol) and high
166 molecular weight PVP (1.3×10^6 g/mol) were prepared by dissolving the polymer in
167 ethanol. For the dye loaded formulations a duplicate solution was made with addition
168 of fluorescein dye at 0.05% w/w of PVP concentration.

169 Solutions of 1 % w/v and 5% w/v low molecular weight PCL (1.4×10^4 g/mol) and high
170 molecular weight PCL (8.0×10^4 g/mol) were prepared by dissolving the polymer in
171 dichloromethane. For the dye loaded formulations a duplicate solution was made with
172 the addition of Rhodamine B (PCL) dyes at 0.05% w/w of PCL concentration. Table 1
173 summarises the eight formulations used in this study and their composition.

174 **2.6. Physical characterisation of polymeric solutions**

175 Physical properties (viscosity, surface tension, electrical conductivity and density) of
176 the solutions were examined. Each parameter was tested in triplicate and an average
177 with standard deviation was then calculated. Surface tension was measured using a
178 torsion balance. (White Electrical Instrument, Worcestershire, UK). A Seven Compact
179 S230 conductivity meter (Mettler-Toledo, Switzerland) was used to measure the
180 electrical conductivity of solutions, where prior to each measurement the probe was
181 calibrated using two standards of 1413 S/cm and 12880 S/cm solutions.

182 Density was obtained using standard 50 mL pycnometers (VWR, UK). Each
183 pycnometer was weighed on an analytical balance, filled to full capacity with the
184 solution and then re-weighed. The difference in weight represented the mass (g) of the
185 solution, which was then divided by the volume (25 mL) to get a density value. The
186 following formula is then used to calculate density (Equation 1).

$$187 \quad \text{Density} = \frac{(\text{Weight of bottle and formulation} - \text{Weight of Empty Bottle})}{\text{Volume (25mL)}} \quad \text{Eq. 1}$$

188 Viscosity measurements were recorded at ambient temperature (20.6 °C) using a SV-10
189 Sine-wave Vibro viscometer (A&D, Japan). Solutions were poured into a plastic holder
190 and the metal vibrators were clamped down when they had reached the surface of the
191 solution. A reading for viscosity was then recorded and the metal vibrators were cleaned
192 using purified water between each new sample solution reading.

193

194 **2.7. EHDA – Coating application**

195 A syringe containing 5 mL of formulation was secured to a syringe infusion pump
196 (Harvard apparatus, pump 11-Elite, USA) which controlled the flow rate of polymer-
197 drug solution. The solution then passed through silicon tubing which was connected to
198 a stainless-steel coaxial needle device (single needle was used in this study) at various

199 flow rates (ranging from 15-50 $\mu\text{L}/\text{min}$). This device was attached to a high-power
200 voltage supply (Glassman High Voltage Supply, UK). The ES/ESP process carried out
201 under ambient temperature of 23 $^{\circ}\text{C}$.

202

203 **2.8. Spraying modes**

204 To assess the various spraying modes, a 5 mL syringe containing solution was ES/ESP
205 at varying voltages (5-15kV) and flow rates (10-80 $\mu\text{L}/\text{min}$) digital images were then
206 taken when different jet formations was observed using a Samsung NX2000 camera.

207

208 **2.9. Preparation of Coated Polymer Microneedles**

209 Microneedles obtained from AdminPatch with an array of 900 needles measured 800
210 μm -tall microneedles located within 1 sq. cm circular area. The entire device is 20 mm
211 in diameter and is made of medical-grade SS316L stainless steel. For the preparation
212 of coated polymer MNs, EHDA was used. The polymeric solution containing the dye
213 was loaded into a syringe fixed to a pump, which allowed the controlled infusion of the
214 solution throughout the system. The syringe was connected to a conducting stainless-
215 steel needle via silicone tubing. The resulting atomised structures were collected on
216 both microscope slides and MNs. Figure 1 shows a schematic diagram of the EHDA
217 set-up.

218

219 **2.10. Imaging analysis**

220 Prior to coating the MNs, solutions containing different concentrations and molecular
221 weights of polymer were atomised at varying flow rates, deposition distances and
222 voltages to assess the morphology and characteristics of the resultant structures. This
223 was according to the QbD DOE experiments. This allowed the most optimal process

224 parameters to be selected for each formulation. SEM micrographs was taken for these
225 samples including the coated MNs. Prior to analysis, samples were gold coated (S150B,
226 Edwards, Crawley, West Sussex, UK) under vacuum and images were obtained using
227 a Zeiss Evo HD-15 (using an accelerating voltage of 5 kV). Working distances between
228 9.5 and 10.5 mm were utilised while applied voltages ranged from 10 to 18 kV with
229 magnifications of x5 k and x40 k; termed as low and high magnifications. The
230 optimised samples were observed at low magnification ($\times 40$) using Leica DME Optical
231 Microscope using XL1 Camera Software.

232

233 **2.11. Contact angle analysis**

234 Contact angle of all 8 formulations were characterised using a ThetaLite T100 contact
235 angle goniometer; using OneAttension software to analyse data. 10 μ L of distilled water
236 droplets were used. Each sample was carried out and assessed in Sessile Drop mode in
237 triplicate and an average was obtained.

238

239 **2.12. Particle size analysis**

240 Particle morphology was assessed via a predetermined scale based upon literature
241 records of what is most suitable. Particle size distribution was carried out following
242 SEM analysis. Smart TIFF software was used to measure particle size and fiber
243 diameter. These measurements were then converted into a percentage and the size
244 ranges were plotted as a bar chart to allow for comparison.

245

246 **2.13. FTIR studies**

247 FTIR was used to analyse all 8 formulations as well as the dyes and raw polymers. Prior
248 to any measurement, FTIR (IRPrestige-21, Japan) background was scanned 10 times

249 and a range of 400-4000 cm^{-1} was determined. The samples were then clamped into
250 place above a dense crystal and scanned ten times. The peaks' wavenumbers were
251 identified and labelled using the Bruker Opus 7.0 FTIR software.

252

253 **2.14. DSC studies**

254 All 8 formulations as well as the dyes and raw polymers were analysed by Jade DSC
255 (PerkinElmer precisely, Shelton, USA) and Pyris Jade DSC software, to analyse
256 thermal transitions. The sample was placed into an aluminium pan and then covered
257 with a lid with holes, followed by crimping. The sample was loaded into the machine
258 and scanned from 20 °C - 300 °C with a heating and cooling rate of 20 °C/min.

259

260 **2.15. *In vitro* release studies**

261 Drug release of the optimised nanoparticles were analysed using UV spectroscopy. A
262 phosphate buffered saline (PBS) medium was used to carry it out. Vials containing 10
263 mL of PBS) and 10 mg of sample (dyes) was constantly stirred at 90 rpm. At
264 predetermined time points, 1 ml of release was retracted and replaced with 1ml of fresh
265 PBS at physiological conditions (37 °C). Drug release was determined using UV
266 spectroscopy absorbance with a set wavelength of $\lambda = 494$ nm (for FL) or $\lambda = 595$ nm
267 (for RhB). This was carried out in triplicate and an average was taken. The data
268 collected from these *in vitro* studies were plotted in different kinetic models to assess
269 the release kinetics of dyes from the atomised polymeric coatings.

270

271 **2.16. *In vitro* diffusion studies**

272 Transdermal diffusion of dyes was assessed using Franz diffusion cells (Copley
273 Scientific, Nottingham, UK) with a diffusion Surface area of 1.77 cm^2 . Strat-M[®]

274 membrane (purchased from Sigma Aldrich) was first punctured with the coated MN
275 manually for a minimum of 10 seconds (up to 30 seconds) until all needles had
276 penetrated/breached the membrane, it was then removed and the membrane was placed
277 between the donor and receptor compartment (which was filled with 12 mL of PBS and
278 a mini stirrer). The Franz cells were maintained at 37 ± 0.5 °C. An aliquot of 1 mL of
279 sample was withdrawn from the receiver chamber at predetermined intervals and
280 replaced with 1 mL fresh PBS. This receiver solution was agitated using a magnetic
281 stirrer at 400 rpm to ensure homogeneity throughout the experiments. In avoidance of
282 evaporation, the donor cells were covered with parafilm. The experiment was carried
283 out in triplicate for each dye loaded MN. The samples were immediately centrifuged
284 following collection at a speed of 14,000 rpm and the supernatant was analysed. UV
285 spectroscopy ($\lambda = 494/594$ nm for PVP/PCL respectively) was used to analyse samples.
286 The cumulative amount of drug permeating through Strat-M[®] was plotted as a function
287 of time.

288

289 **2.17. Confocal laser scanning microscope imaging studies**

290 The permeation experiment was carried out for each dye loaded MNs. After 24h, the
291 formulations were removed from the donor compartment and the Strat-M[®] membranes
292 were removed and wiped gently from the Franz cells. The membranes were placed
293 immediately on a glass slide, covered with a glass slide and examined with laser
294 scanning confocal microscope [46]. Z-stack images were acquired by stepwise
295 scanning of each membrane from its top to the equatorial plane at 1.16 μm steps with a
296 63 \times oil-immersion lens under a Zeiss LSM 780 CLSM (Carl Zeiss Microscopy GmbH,
297 Berlin, Germany) with the appropriate filters. Images were obtained with ZEN 2011
298 software.

2.18. Insertion test of the coated and non-coated MNs

The sufficient insertion ability of the coated MNs is imperative for effective drug delivery into the skin. In the present study, the insertion studies of the uncoated MNs and the coated MNs were performed by using a Testometric tensile test machine (UK) and Parafilm M[®] (Bemis Company Inc., Soignies, Belgium). Parafilm M[®] was folded eight times to simulate the thickness of the skin and the MN array was placed onto the movable cylindrical probe with a double-side adhesive tape. The MN arrays were inserted at a speed of 0.5 mm/sec, into the Parafilm layers by applying a force of 40 N for 30 sec. After insertion, the Parafilm layers were unfolded and the number of holes in each layer was counted using an optical microscope (Celestron MicroDirect 1080p HD Handheld Digital Microscope, Celestron, Torrance, California, USA).

310

3. Results and Discussion**3.1. Evaluation of EHDA process using QbD**

The purpose of the first set of experiments was to ascertain which of the two concentrations and molecular weight of polymer should be selected for the production of particles and fibers for each polymer using EHDA (Figure 1). The solutions that were prepared as described in Table 1 were formulated again and each experiment was ES or ESP in the order shown in Figure 2A and B. The factors and responses were put into JMP Pro software and the software generated a table of runs which is displayed in Figure 2. The rationale for these experiments was to produce a full factorial design, whereby parameters that show no desirable responses are eliminated from the remaining DOE providing the next set of experiments.

Once the screening design had been performed and the results analysed, a further verification study was performed. The factors being investigated and their subsequent

324 ranges were defined further and there were no great variations in the data range. Four
325 sets were carried out, two for the different polymer particles and two for the different
326 polymer fibers. The deposition distance being investigated were 10, 12.5 and 15cm;
327 and 15, 20 and 25 $\mu\text{L}/\text{min}$ were the flow rates being looked at for PVP particles and for
328 PCL it was 12.5, 15 and 20 cm; and 20, 40 and 60 $\mu\text{L}/\text{min}$. As can be seen from the
329 initial results, the mean particle size for the majority of the runs were below 500nm as
330 well as the polydispersity results also being low for both particles and for fibers it was
331 within the micron range.

332 Once the parameters for the particles and fibers were obtained the second set of
333 experiments for PVP and PCL were carried out. The resultant particles/fibers deposited
334 were then assessed using imaging as well as thermal and spectroscopic techniques. The
335 prediction profilers in Figure 2C-F predict the optimal work space regions for the three
336 dependent variables. The response surface plots for particle size are shown in Figure
337 3A-D and the response surface plots for particle shape and polydispersity can be found
338 in supplementary materials. The implementation and analysis of a response surface
339 fractional factorial DOE with a reduced number of runs helped to identify the effects of
340 the selected independent variables and identify those settings for particles and fibers of
341 optimized quality. The jetting images shown in Figure 4 depicts the various spraying
342 modes. Figure 4A-P show the jetting modes for each formulation.

343 The appearance of the resulting structures was consistent with all experimental runs
344 producing spherical particles (Figure 5A, B, I, J). High molecular weight PVP shows
345 larger sized structures all within the micrometer range (Figure 5K, L). The
346 polydispersity was also higher with this polymer. The mean particle size was selected
347 as being less than 500 nm; because the aim is to produce nanoparticles any particles
348 produced that are either at this value or lower will meet the criteria that is set in the

349 QTPP. It has also been stated that nanocarriers that fall into the range of 50-500nm are
350 generally acceptable; it has also been shown that polymeric particles that are <500nm
351 in diameter have a general higher intracellular uptake rate. [47]

352 At a low flow rate, an array of fibers was produced with varying fiber diameter due to
353 the higher viscosity of the solution. As the flow rate increases, the formation of fibers
354 reduces at the same time as the development of agglomerated material begins to
355 intensify; particularly in Figure 5G. This is due to the short drying time causing non-
356 evaporation of the solvent and low stretching of the solution in the flight between the
357 capillary tip and collector.

358 Optical images were taken of the finalised formulations which can be seen in Figure
359 5A-H. The final optimised particles (PVP particles Figure 5I and 5J, PCL particles
360 Figure 5M and 5N) and fibers (PVP fibers Figure 5K and 5L, PCL fibers Figure 5O and
361 5P). According to the ICH Q8 guidelines a design space can be defined as “the
362 multidimensional combination and interaction of input variables (e.g. Material
363 attributes) and process parameters that have been demonstrated to provide assurance of
364 quality”. When working within the designated design space, any change here is not
365 considered by the regulatory authorities as a change in the process therefore this can
366 lead to more flexibility. However; movement out of the design space is considered to
367 be a change and would normally require regulatory approval. Working within the
368 design space guarantees product quality which therefore in turn makes sure that the
369 manufacturing process is robust as well as generating additional financial benefits as
370 there is a reduction in cost as there are less batch failures.

371 Stability studies of the coated microneedles over time are presented in Figure S1. The
372 resultant particles and fibers were assessed over 10 days. The PVP particles (F2) and
373 the PCL particles (F6) showed no significant morphological changes with no signs of

374 degradation over a period of 10 days. The same trend was observed with the fibrous
375 structures (F4 and F8). Figure S1 shows the resulting structures at high magnification.
376 Here, the structures have evidently kept their shape and there is no evidence of any
377 morphological changes which is consistent with findings shown in Figure 7. This
378 proves the integrity of polymers and dye and shows that the atomised structures
379 remained intact and stable for an appropriate time period. This also highlights the
380 benefits of the EHDA process; showing that this engineering process is capable of
381 fabricating structures of advantageous morphological and structural stability.

382 In order to establish a design space the contour profile must have at least two active
383 factors. As can be seen from Figure 3 the prediction profiler flow rate was shown as
384 being an active factor. Therefore in order to obtain a design space for verification studies
385 deposition distance was added to the profile as an active factor. The design space is the
386 white region in the figure and when a process is carried out in this area then producing
387 a product whereby quality is assured.

388 Flow rate is the only factor that is being shown as having an effect on polydispersity.
389 The p-value is also less than 0.05 indicating that it is important and that an interaction
390 is taking place between polydispersity and the responses being investigated.

391 Furthermore, the polymers selected demonstrate options for both burst release (PVP)
392 and sustained release (PCL). These polymers have been previously in clinical trials and
393 in current drug dosage form development [48,49]. The study carried out here with these
394 common, compatible polymers also provides imperative evidence that different,
395 potentially personalised structures can be engineered using a method that can be easily
396 optimised for upscaling.

397

398 **3.2. Physical characterization of solutions**

399 As can be seen in Table 2, the general trend for both high and low molecular weight
400 PVP is that as the concentration of the polymer increases so does the recorded electrical
401 conductivity. The results for electrical conductivity for low and high molecular weight
402 PVP at 5% w/v were all very similar and fell into a very narrow range (3.01 $\mu\text{S}/\text{cm}$ and
403 2.65 $\mu\text{S}/\text{cm}$ respectively).

404 Faraji et al study found that the overall stability of the spraying process is dependent on
405 the electrical conductivity of a sample to a certain extent. It is also believed that an
406 increase in conductivity leads to smaller droplet sizes which occur because during the
407 process there is more of a charge in the liquid solution [50]. Table 2 shows that 1% w/v
408 1.4×10^3 g/mol- PCL acquires the highest conductivity value at 7.82 $\mu\text{S}/\text{cm}$ and 5% w/v
409 8×10^3 g/mol-PCL with the lowest conductivity value at 6.39 $\mu\text{S}/\text{cm}$.

410 As the viscosity of the solution increases, the surface tension decreases as represented
411 in Table 2 and further confirmed by Abel whom studied the electrospinning of PCL
412 [51]. DCM has shown compatibility with PCL carriers in studies conducted by Xie et
413 al [52]. DCM has a low viscosity of 0.44 $\mu\text{S}/\text{cm}$ and low density of 0.166 g/mL and
414 hence has a very insignificant impact on the overall viscosity of the solution.

415 The formation of fibers is often seen because as the molecular weight of the polymer
416 increased so did the viscosity. This is also to be expected as molecular weight reflects
417 the entanglement of the polymer chains and a higher molecular weight meaning the
418 chains are more rigid and held more tightly together so the viscosity will be much higher
419 when comparing it to lower molecular weight polymers. Similarly, to the electrical
420 conductivity results although error bars were added to the graph they do not show
421 because the standard deviation was far too low at 0.0058 and 0.0153 respectively.

422 Similarly, to the trend observed in the Table 2 as the concentration of both the high and
423 low molecular weight polymer increased so did the density. The density of polymer

424 solutions is another important factor that can influence the EHDA process as it dictates
425 whether particles or fibers are going to be produced. It has been thoroughly researched
426 and found that the critical polymer concentration (C_{ov}) can influence the formation of
427 particles. The critical concentration of each polymeric solution can be found; this is
428 when the polymer chain begins to overlap and entangle. In order to produce particles, a
429 low entanglement density is required [53].

430 Surface tension of a polymeric solution is also another important factor that influences
431 the EHDA process. EHDA is only able to occur when the electric stress is able to
432 overcome the surface tension to form a stable cone jet. This charge repulsion is the
433 rationale for the particle breakdown into nano-sized particles, as the liquid is ejected
434 from the capillary needle and accumulated on the collection plate. The surface tension
435 must be lower than 50 N/m for a liquid to be atomised under the influence of electrical
436 field. The electrical stress must overcome the surface tension to achieve a stable cone-
437 jet. As the surface tension was below this value (50 N/m) for both high and low
438 molecular weight PVP solutions at 0.038 and 0.018 mN/m (high molecular weight PVP
439 at 1% and 5% w/v) and at 0.015 and 0.031 mN/m (low molecular weight PVP at 1%
440 and 5% w/v), it can be assumed that either molecular weight of polymer and
441 concentration (if based solely on surface tension alone) can be used for the EHDA
442 process.

443

444 **3.3. Spraying modes**

445 Research suggests the most typical spraying modes include dripping, spindle, cone-jet,
446 multi-jet modes depending on the geometrical form of the liquid drop formed at the
447 meniscus/jet at the outlet of the capillary. Other modes of spraying recorded include
448 micro-dripping, multi-spindle, ramified meniscus, oscillating jet and precession have

449 been observed similarly with a single capillary but dependent upon the liquid and
450 process parameters [54].

451 The fundamental principle of EHDA involves a liquid emerging from the nozzle under
452 the action of surface tension being subjected to an acceleration force in the form of an
453 electric field. A variety of oscillating behaviours reported in Figure 4 which portrays a
454 range of modes (dripping and jetting). The modes can be very clearly differentiated.

455 The polydispersity index (mean particle size and uniformity of particle size in the
456 distribution can be seen in Figure 4A depends on the spraying mode. The ES droplet
457 can vary from few hundred nanometers to micrometers. Therefore, the physical
458 properties of the solution and experimental design is paramount in the determination of
459 the spraying mode. The EHDA set up was done so with the attachment of a high-speed
460 camera to capture real time live footage of electrospaying and electrospinning in
461 action. Stable cone jets were observed with Figure 4N. The modes were observed from
462 micro-dripping to Taylor cone, as the voltage increases. The map highlights the various
463 regions which includes the different spraying modes and the stable jetting regions. It is
464 in the stable jetting region where a stable cone jet is formed and the resultant spray will
465 lead to the deposition of atomised nanoparticles. The lower viscosity solutions (low
466 polymer weight and lower concentration) yielded smaller droplets and lower
467 polydispersity [55]. The opposing characteristics were found with higher molecular
468 weight and higher concentration polymeric solution, which led to electrospinning with
469 the system [56].

470 Figure 4J represents the ‘dripping’ mode, which arises when no voltage is applied.
471 Regular, large droplets detach from the capillary to form drops as the electrical force
472 and the weight of the drop overcomes the capillary forces. With a voltage increase,
473 the meniscus elongates and the drop be-comes smaller. The most efficient mode of

474 attaining a narrow particle size distribution is the ‘cone-jet’ mode, also known as the
475 stable Taylor cone (Figure 4N). The liquid forms a cone with a thin jet at its apex
476 where the liquid elongates into a long, fine jet and then fragments into droplets under
477 the influence of electrostatic forces. Figure 4P illustrates a ‘multi-jet’ mode where the
478 meniscus flat-tens with small cones at separate points at the circumference of the
479 capillary, whereby fine jets of liquid are ejected. The ‘precession’ mode occurs when
480 the liquid escapes the capillary in the form of a skewed cone and changes into a thin
481 jet at its apex (Figure 4I-N). This mode differs from ‘cone-jet’ as the jet in the
482 ‘precession’ mode rotates around the capillary axis.

483 As seen in Figure 4, the formulations containing dye as opposed to polymer alone had
484 distinctive differences. In Figure 4C and Figure 4A there is one consistent unstable
485 region. There was better stability below 15kV. Whereas, in Figure 4D the higher
486 molecular weight polymer with fluorescein dye has a very different jetting map
487 compared to Figure 4B. With F4, the jetting map shown in Figure 4D shows 2 unstable
488 regions making it more problematic to fabricate fibers.

489 For the PCL formulations, similar behaviour was shown whereby Figure 4E, 4F, 4G
490 and 4H have one unstable region. There is also a larger stable jetting region. Whereas
491 Figure 4F has a large unstable jetting region compared to Figure 4E where there is only
492 a small unstable jetting area for PCL alone. Again, with Figure 4H there are two large
493 unstable jetting regions. It also shows more stable jetting at higher voltages as the flow
494 rate increases.

495 **3.4. Optical microscopy studies**

496 Optical microscopy results show small spherical near uniform particles for both F1 and
497 F2 as shown in Figure 5A and B. Whereas in the optical images for the higher molecular
498 weight formulations Figure 5C has smoother fibers and the PVP-FL fibers shown in

499 Figure 5D has smooth looking fibers with some beading. This could be due to
500 formulation instability as well as some instability experience during the electrospinning
501 process. This was further confirmed with SEM.

502 With the optical images obtained for PCL the PCL particles sprayed and shown in
503 Figure 5E the particles are slightly less spherical with some particles agglomerating.
504 Figure 5F shows a larger distribution of particles with some near spherical again with
505 some agglomeration. This can be due to the rapid solvent evaporation as DCM is a very
506 volatile solvent. In Figure 5G there are many beaded fibers with the PCL formulation
507 with more unstable electrospun fibers shown in Figure 5H.

508

509 **3.5. SEM studies**

510 Figure 5I-P displays the optimised particular and fibrous structures following QbD
511 implementation and DOE analysis. Figure 5I shows uniform, spherical PVP particles
512 and this is similar with the dye loaded PVP-FL particles. Figure 5J was produced at a
513 flow rate of 15 $\mu\text{L}/\text{min}$ flow rate and a deposition distance of 15cm were chosen as the
514 optimum conditions to spray. Although the results from JMP show that deposition
515 distance is not an influencing factor literature shows that a greater distance results in
516 smaller particle size; therefore, a deposition distance of 15 cm was selected. Below is
517 an SEM image of the optimised nanoparticles. Similarly, smooth PVP fibers can be
518 seen in both Figure 5K and 5L with the size of fibers measuring very similar. The
519 optimised fibers were produced at a flow rate of 20 $\mu\text{L}/\text{min}$ at a deposition distance of
520 10 cm and the mean fiber size measuring 4.5 μm . The PCL samples were quite
521 problematic to spray initially due to issues with solvent evaporation and agglomeration.
522 However, following DOE analysis, 1.4×10^3 g/mol-PCL, 5% w/v PCL, a flow rate of 15
523 $\mu\text{L}/\text{min}$ and a deposition distance of 15 cm produced nanoparticles with a mean size of

524 209nm. The PCL fibers produced in Figure 5O and 5P appear smooth with even
525 distribution compared to that found in the optical images, as these were more stable and
526 produced at optimal conditions at a deposition distance of 10 cm and flow rate of 50
527 $\mu\text{L}/\text{min}$.

528 Figure 6 displays the morphology of coated MNs with all 8 formulations. Figure 6A
529 shows sparsely coated MNs with the majority of the coating concentrated at the tips
530 (F1). This is quite similar to what was found with F2. This can also be due to the
531 deposition distance during the spraying process. Figure 6C and 6D display the PVP
532 fiber coated MNs (F3+F4), with the dye loaded MNs appearing as dense as the polymer
533 alone. The fibers appear very dense and smooth on both with Figure 6E and 6F showing
534 a more even coating with PCL particles. The dye loaded F6 PCL particles appear more
535 densely coated (Figure 6F) and Figure 6G shows beaded fibers were present with the
536 polymer alone however more dense coatings with less beading is seen in Figure 6H.

537

538 **3.6. Size distribution of particular/fibrous structures**

539 The particle size distribution graph for ES PVP and PCL particles shown in Figure 7A
540 are negatively skewed which is desirable. The majority of particles were within the
541 nano size range and this coincides with the polydispersity whereby this value reflects a
542 narrow nanoparticle size distribution with the value closer to 100 nm. This can be seen
543 as important parameters in the QTTP profile (Table S1, S3) and so is a major factor in
544 DOE analysis and the response surface profiles. The average particle size for F1, F2,
545 F5 and F6 were $0.39 \mu\text{m} \pm 0.0791 \mu\text{m}$, $0.45 \mu\text{m} \pm 0.0404 \mu\text{m}$, $0.57 \mu\text{m} \pm 0.0256 \mu\text{m}$
546 and $0.63 \mu\text{m} \pm 0.0435 \mu\text{m}$, respectively. There was a significantly larger proportion of
547 PCL particles (F5 and F6) within the larger size ranges which could be due to
548 agglomeration as a result of rapid solvent evaporation experienced with DCM.

549 However, on the whole there was a larger frequency of PVP and PCL particles within
550 the smaller size ranges. Research supports these findings as particles with small size
551 distributions have a high level of effectiveness in their application.

552 The average fiber diameter for F3, F4, F7 and F8 $1.11 \mu\text{m} \pm 0.034 \mu\text{m}$, $1.13 \mu\text{m} \pm 0.058$
553 μm , $1.19 \mu\text{m} \pm 0.068 \mu\text{m}$ and $1.27 \pm 0.053 \mu\text{m}$. The fiber diameter graph shows even
554 size distribution within the nano and micro range (Figure 7B) which enables them to
555 mimic the extracellular matrix.

556

557 **3.7. Contact angle goniometry studies**

558 Contact angle (CA) has a major impact on drug release from a device/system and the
559 materials surface is the first point of contact with the biological surroundings. It
560 provides quantitative measurements of the wetting of a solid which is liquid (water is
561 commonly used) Angles lower than 90° indicate high wettability whilst angles larger
562 than 90° indicate poor wettability. CA was necessary in this study to measure the
563 interaction between the polymeric coatings alone and when included with a dye as these
564 varied in structure (particular/fibrous) they would determine the release and detachment
565 from MNs (Figure 8). The wettability of the surface of the electrically atomised samples
566 were characterised and analysed over time. This included hydrophilic (PVP) and
567 hydrophobic (PCL) particles and fibers making it a potential carrier drug delivery
568 system providing controlled rapid/sustained drug release.

569 It has been reported that with increasing molecular weight of PVP that the density
570 increases and the water content decreases. This supports the findings in Figure 8. F3
571 and F4 are the higher molecular weight PVP samples and the contact angle
572 measurements as seen in Figure 8A is much higher at 0 seconds (14.98° and 39.01°)

573 respectively) in comparison to the lower molecular weight PVP F1 and F2. PVP is a
574 more hydrophilic polymer hence the rapid dissipation.

575 PCL has gained its notoriety being easily accessible, easy to process, good mechanical
576 strength and biodegradation. From the results it is apparent that compared to the PCL
577 polymer alone the dye inclusion further increased the contact angle. This is due to the
578 hydrophobicity of PCL which was improved when modified. Its hydrophobicity has a
579 whole host of effects including the adherence of proteins onto a surface thus suggesting
580 optimal contact angle measurements needed for certain applications. Although the
581 surface tension did not vary massively between the PCL formulations, the contact angle
582 for fibers was lower with F8 as their fiber diameter increased more so than F7. F8 is
583 classed as super hydrophobic. The higher CA values in comparison to PVP can also be
584 due to PCL stability and resistance to degradation by the deionized water. It's been
585 reported that the test medium, porosity and test medium can all significantly impact CA
586 behaviour.

587

588 **3.8. FTIR studies**

589 The FTIR spectrum shown in Figure 9A is that of the pure PVP. Peaks at 3418.88 cm^{-1}
590 1 (O-H stretch), 2955 cm^{-1} (C-H asymmetric stretch), 1644.36 cm^{-1} (C=O stretch),
591 $1421.22\text{ (CH}_2\text{)}$ and 1285.69 cm^{-1} (C-N vibration) are identified which correspond to the
592 structure of PVP.

593 Figure 9A also displays the spectrum obtained for pure fluorescein and the following
594 peaks identified in the spectrum confirm that the sample being analysed is that of
595 fluorescein. 1636 cm^{-1} (C=O symmetric stretch), 1588.4 cm^{-1} (COO⁻ asymmetric
596 stretch), 1457.23 cm^{-1} (C-C stretch), 1366.47 cm^{-1} (C-C stretch) and 1108.08 cm^{-1} (C-H

597 aromatic in plane bend). These peaks and bonds were also identified in an article by
598 Wang *et al.*, when they too were analysing raw fluorescein [54].

599 The optimised nanoparticles significant peaks include; 3416.14 cm^{-1} (OH stretch),
600 2953.05 cm^{-1} (CH asymmetric stretch), 1651.33 cm^{-1} (C=O stretch), 1460.96 cm^{-1} (C-C
601 stretch) and 1422.26 cm^{-1} (CH_2 bend). When comparing the spectrum for pure PVP and
602 the optimised nanoparticles they appear to be very similar and the majority of the peaks
603 that were seen in the spectrum for PVP are also visible in the spectrum for the optimised
604 nanoparticles. The peak at 1460.96 cm^{-1} corresponding to the C-C bond is also present
605 in the fluorescein spectrum which can therefore lead to the assumption that fluorescein
606 and PVP have encapsulated together. The peaks also appear much broader and well
607 defined which is often seen in a spectrum when two or more components are believed
608 to be mixed.

609 In Figure 9B, the characteristic absorption peak at 1730 cm^{-1} is the major transmission
610 peak of PCL and arises due to the carbonyl stretching of the C=O. The bands at 2943,
611 1293, 1238, 1164, 1107 and 1045 cm^{-1} which correspond to asymmetric CH_2
612 stretching, C-O and C-C stretching in the crystalline phase, asymmetric COC
613 stretching, OC-O stretching, symmetric COC stretching and C-O and C-C stretching
614 in the amorphous phase, respectively. The major peaks are confirmed by Gurlek et al.
615 in 2017 [56]. In Fig. 13b, the weak intensity band at 3085 cm^{-1} denotes to aromatic C-
616 H bonds, which also arises at 1335 cm^{-1} (plane bending), 815 cm^{-1} (out of plane
617 bending) and at 681 cm^{-1} (wagging vibrations). The peaks at 1691 cm^{-1} and 1644 cm^{-1}
618 are associated with the vibrational stretching of C=N and C=O, respectively. The
619 strong band at 1583 cm^{-1} is due to the asymmetric stretching of the COO- group which
620 is further confirmed by the band at 1469 cm^{-1} , ascribed to symmetric stretching of the

621 group. The aromatic C-C stretch is observed at 1335 cm^{-1} and the C-O results from
622 the 1245 cm^{-1} peak. The major peaks are confirmed by Dukali et al. in 2014 [57].
623 In addition, the F6 spectra can confirm the interaction between the selected polymer
624 PCL and model compound, RhB. Large similarities between the PCL and F6 and F8
625 spectra appear. This is due to the RhB becoming encapsulated within the polymeric
626 chains, thus we can observe absorbance resemblances between them. The following
627 transitions in the peaks (peak shifts and broadening) indicate successful interaction
628 between PCL and RhB; the peaks at 2933 cm^{-1} and 1100 cm^{-1} became broader and
629 could be due to the interaction of the peaks of unprocessed RhB at 1583 cm^{-1} and
630 $1073\text{-}1175\text{ cm}^{-1}$, respectively. Additionally, a peak formed at 801 cm^{-1} which is due
631 to the several absorbance at and around 779 cm^{-1} , shown in unprocessed RhB.

632

633 **3.9. DSC studies**

634 Figure 10A displays the DSC thermogram for pure PVP. As can be seen from the
635 thermogram there is a distinctive peak at $120\text{ }^{\circ}\text{C}$ which represents the melting
636 temperature of the sample. In many sources of literature, it is stated that the melting
637 point of pure PVP should fall in the range of $150\text{ }^{\circ}\text{C}$ - $180\text{ }^{\circ}\text{C}$; however, the melting point
638 recorded does not show this and appears to be out by $30\text{ }^{\circ}\text{C}$. The sample for pure PVP
639 was analysed again to make sure that the recorded melting point was not an anomalous
640 result; but after repeating this particular run a further two times the melting temperature
641 of $120\text{ }^{\circ}\text{C}$ was still recorded.

642 This slightly lower melting point value may have been recorded and explained by the
643 fact that the PVP being tested had a molecular weight of 40K; and it has been noted that
644 the molecular weight of a polymer can affect the melting point. This is because an
645 increase or decrease in molecular weight can influence the overall flexibility and/or

646 rigidity of a polymer which can therefore in turn have an effect on the polymers melting
647 point.

648 The melting point for fluorescein is above 300 °C and a clear endothermic peak is
649 visible at 340 °C for FL. It can be seen from the thermogram there is also only one
650 single peak representing the melting point; this observation can be to a certain extent
651 be linked to the purity of the sample as there are no other peaks or interactions being
652 shown. Making sure that the starting materials themselves at the start of a process are
653 pure and therefore of the desired quality is very important when implementing a QbD
654 approach; as in order to make sure that the end product is of exceptional quality each
655 aspect and unit operation of the manufacturing process must also conform to a robust
656 and high-quality procedure.

657 For the optimised nanoparticles the thermogram a single endothermic peak is visible at
658 approximately 120 °C. This melting point is the same as is seen on the raw PVP
659 thermogram; therefore, it can be assumed that the PVP and fluorescein dye have fully
660 encapsulated and have formed a single entity.

661 DSC provides thermal information about the materials used to facilitate in the
662 identification and verification of excipients. DSC results, presented in Figure 11B,
663 show a single melting peak with a maximum melting temperature (T_m) of unprocessed
664 PCL of ~ 62°C. The T_m of unprocessed RhB is ~ 208 °C and can be seen on the
665 thermogram.

666 However, a second broad peak is observed at ~ 265 °C. The phenomenon of double
667 melting peaks is due to the impartial melting and recrystallisation of the crystallite at
668 that specific moment of thermal scanning. The T_m and second peaks are associated
669 with the melting of imperfect and perfect crystallite, respectively [58]. The T_m of F6
670 and F8 spectra is shown to be slightly decreased (~53 °C), implying that smaller

671 crystallites are formed during EHDA and successful encapsulation of RhB within
672 PCL.

673

674 **3.10. *In vitro* release studies**

675 *In vitro* release study results are shown in Figure 11. The PVP particle (F2) formulation
676 displayed 100% of FL dye was released within 120 minutes (2 hours) with initial burst
677 release similar to the trend shown with (F4) PVP fiber formulations as FL dye showed
678 100% release within 300 seconds (5 h). At 120 minutes, the proportion of drug released
679 was 100%; this satisfies the original QTPP where 75% or more of the drug should have
680 been released before 4 h. At 30 min, approximately 94% of the drug had been released
681 for both F2 and F4; after this point, a plateau had reached as the majority of the drug
682 had already been released. These results are similar to what is reported in literature.
683 Rapid release profiles are associated with PVP with one study reporting up to 100%
684 drug release with PVP coated formulations within 15 min [59]. The slightly longer
685 delay can be attributed to FL. The error bars displayed on the graph above are also
686 narrow suggesting that there was little variation when performing each individual test
687 run and this suggests that the results obtained are both reliable and reproducible.

688 RhB possesses a distinctive and strong absorption peak, which offers an accurate
689 concentration analysis using UV spectroscopy. The initial burst (1 minute) of shows a
690 ~ 44% of RhB being released, which can be observed in Figure 11A. An initial burst
691 resulted from the large surface area to volume ratio of the NP, in addition to the surface
692 loading of RhB. From 2 – 10 min, the release gradually increases from ~ 44% to 52%.
693 After 10 min, the drug released slowly with a total of ~ 75% released after 4 h. The
694 delayed release was due to the opposing effects of the hydrophobicity of PCL and
695 hydrophilicity of RhB. This hindered the release of RhB thus presenting a sustained

696 release profile. Moreover, the QTPP necessitated a sustained release of RhB over a
697 minimum of 7 days. Approximately, 100% of RhB was released after 7 days, which
698 resonates with the QTPP target for the release profile. The release profile was further
699 confirmed by Cao et al in 2014 where the release profile of RhB from PCL/PLGA was
700 measured in a study investigating the ‘dual drug release from core-shell nanoparticles
701 [60]. At 7 days, the EE and DL were measured. The calculated values were 65% and
702 0.6%, respectively. The target EE as stated in the QTPP is > 85%, however only 65%
703 of RhB was successfully encapsulated in PCL. This may be because of the unstable jet
704 during ES and ESP, resulting in loss of particles and beaded fibers. The rapid release of
705 PVP formulations in comparison to the sustained release profiles shown with PCL has
706 support from the well documented research of these polymers within the research
707 community.

708

709 **3.11. Release Kinetics**

710 The data from the in vitro release of dyes was applied to different kinetic models to
711 determine the most prominent mechanism of dyes from the ES/ESP particles/fibers.

712 The data was fitted to zero-order, first-order, Higuchi and Korsmeyer-Peppas models
713 with the regression values and relevant component values being recorded and the
714 corresponding plots seen in Figure 11B-E.

715 Drug diffusion must occur in one direction with the initial drug concentration in the
716 polymeric matrix must be higher than the solubility of drug. The swelling capability of
717 the polymeric matrix and dissolution must be negligible and the drug particles must be
718 smaller than the matrix. If perfect sink conditions have been met as well as the set
719 criteria then the Higuchi model can be applied.

720 The Korsmeyer-Peppas model is most useful when there are multiple release
721 mechanisms involved. A release exponent, n , determines the mechanism of drug
722 release. There can be various n values and each depict specific release mechanisms ;
723 $n \leq 0.45$ corresponds to quasi-Fickian drug transport, $n = 0.5$ shows Fickian diffusion
724 (molecular diffusion of drug due to a chemical potential gradient), $0.45 < n < 0.89$
725 relates a Non-Fickian diffusion mechanism, $n = 0.89$ relates to the case II transport with
726 $n > 0.89$ corresponds to the super case II transport [61].

727 The low R^2 values (Table 3) obtained from zero-order and first order models suggest a
728 poor fit for this type of release kinetics. There were relatively higher (close to 1)
729 R^2 values for all 4 formulations from Higuchi model analysis which suggests the dyes
730 were released via Fickian diffusion; more specifically quasi-Fickian diffusion. From
731 applying the release data to Korsmeyer-Peppas model the n values for F6 and F8 fall
732 between the 0.5-0.89 ranges and so indicates anomalous case II transport kinetics. The
733 n values for F2 and F4 is >0.89 so it is considered as super case II non- Fickian diffusion
734 [32]. Korsmeyer equation supports the findings for F2 and F4 which have very high
735 (close to 1) n values with research of release from hydrophilic polymers like PVP and
736 the ratio of tracer/excipient. In particular the role of the dynamic swelling and
737 dissolution of the polymeric matrix on the release mechanism [61].

738

739 **3.12. SEM analysis of Strat-M[®] membrane and coated microneedles post** 740 **insertion**

741 Figure 12 displays SEM micrographs of the Strat-M[®] membranes and the coated MNs
742 that were used for permeation studies. The micrographs show the morphology of the
743 synthetic membrane as well as MNs post insertion. In Figure 12A the membrane
744 appears very smooth and from the side the layers are visible. The pierced membranes
745 in Figure 12Bi), Ci), Di), Ei) show that cavities have been created as the inset pictures

746 show clear holes created by the microneedles whereby the coating is able to permeate
747 through for permeation and drug delivery. As seen in Figure 12Bi) and Di), there was
748 a limited number of particles surrounding the pierced craters that have been formed;
749 showing the coating had not accumulated here.

750 In comparison to human skin synthetic membranes offer many advantages including
751 controlled membrane thickness, rapid preparation time, more economic and less storage
752 space. Human SC is usually the rate-limiting step for successful Active Pharmaceutical
753 Ingredient delivery (API). Strat-M[®] has been designed to encompass similar structural
754 and chemical characteristics found in the human epidermis. This is via the layers in
755 Strat-M[®] which has a thickness of 300µm. The top layer being supported by 2 layers
756 of porous polyether sulfone (PES) on top of one single layer consisting of polyolefin
757 (non-woven fabric). These multiple layers mimic the layers of human skin. Skin
758 contains various lipids, phospholipids and ceramides, which provides hydrophobicity
759 to skin. Similarly, the membrane contains a combination of lipids (cholesterol,
760 ceramides, free fatty acids and other components) in a specific ratio which is similar to
761 human SC, thus enabling it to be considered as a strong alternative to human skin for
762 permeation studies [62]. Alison et al demonstrated a similar permeation profile of
763 Rivastigmine using Strat-M[®] compared with pig ear skin [63].

764 The MNs post insertion shows sparse coating on the majority of MNs. The tips show
765 no coating. There are some particles on Figure 12C and 12G below the tip suggesting
766 not all of the formulation was able to penetrate through the film. MNs hosting fibrous
767 coatings however showed no coating remaining on the MN tips. There is a very small
768 amount of particular-fibrous structures remaining but this supports the phenomena
769 whereby upon insertion, the fibers are dragged through the skin. The integrity of MNs

770 was significantly different with each MN. MNs coated with F6 (Figure 12G) shows
771 agglomeration of particles potentially due to rapid solvent evaporation.

772

773 **3.13. Permeation studies**

774 Permeation studies of dyes across a synthetic skin membrane (Strat-M[®]) *in-vitro* was
775 carried out using coated stainless-steel microneedles. The conclusion of the experiment
776 led to the production of graphs displaying the cumulative amount of model dye
777 permeating the membrane over time (Figure 13). There was a significant difference in
778 the permeation of PVP fibers in comparison to the other formulations and this can be
779 attributed to molecular dispersion of dye within PVP. With the fast swelling of porous
780 nano-sized fibers and large surface area allowing the fluorescein dye to leach out.
781 Research carried out by Ronnader et al supports the findings with a similar release
782 profile with higher molecular weight PVP and sumatriptan loaded MNs [64]. It was
783 also reported that there was a two fold increase in cumulative drug release over a 24 h
784 period by increasing the sumatriptan succinate concentration by a factor of two [65].

785 *In vitro* release is not the only issue that can have an impact on skin permeation of a
786 drug. It is also possible that the interaction of the nanoparticles with the SC is
787 responsible for the greater or smaller increase in drug skin permeation. An array of
788 research has been carried out with respect to the behaviour of surfactants and oleic acid
789 as permeation enhancers. Oleic acid has the ability to interact with the ceramide head
790 groups of the SC destroying the hydrogen bonding of the lipid bilayers and in turn
791 enhancing drug skin permeation [66,67].

792 Hence, structures with two different morphologies were engineered using the same
793 materials. The release study data reflects the effects of particulate and fibrous structures
794 on the controlled release of the encapsulated probe. One limitation or challenge that is

795 met when utilising MNs as drug delivery device is powder/particle residue on the metal
796 surface post insertion [69]. Fabricating fibrous structures will promote entanglement
797 and forces the coating to be drawn into the pores made by the metal MNs; as seen in
798 Figure 12. The fibrous system could potentially delay the closure of the pores; ensuring
799 the channels are kept open for a longer period of time; increasing drug retention time
800 and hence sustaining drug release. Furthermore, fibrous coatings engineered using
801 electrospinning are easier to manage and handle with being able to control deposition
802 of the resulting structure [69]. It is evident from extensive research surrounding EHDA
803 process synthesises that highly charged droplets and hence charged structures [5]. This
804 can potentially result in repulsion between surfaces of similar charge, ergo fabricating
805 a non-uniform coating, regardless of charge dissipation upon deposition [70-71]. It is
806 important to note here the overall MN coating has the same quantity of particles and
807 fibers required by mass. With respect to particulate deposition, there will be some
808 evident differences when compared to fibrous systems as the latter are more stable [72].
809 With particle engineering using EHDA, deposition time is significantly increased and
810 with dense coating there is a high probability of static build up; which can be overcome
811 by using grounded electrodes [73].

812

813 3.14. Confocal laser scanning microscope imaging

814 The distribution of Fluorescein and Rhodamine-B in the Strat-M[®] membrane was
815 visualized confocal laser scanning microscopy (CLSM). The strong green signal is
816 attributed to the fluorescein while the red signal is attributed to Rhodamine-B. CLSM
817 is often used as an imaging technique for further information about transdermal
818 permeation such as the extend and the penetration route. Figure 14 demonstrates Z stack
819 images of the Strat-M[®] membranes pierced with (A) F2, (B) F4, (C) F6 & (D) F8 MNs.

820 High fluorescence intensities were maintained across the membrane in all formulations
821 while F8 and F4 seem to have a more intense signal especially in lower depth. CLSM
822 imaging indicates the high potential of the investigated MNs for transdermal delivery.
823 Moreover, Figure 14c reveals the size and shape of the MNs while the tip of the
824 microneedle reaches the lowest depth ($z=10$).

825

826 **3.15. Insertion studies**

827 The insertion ability of the coated and non-coated MNs was evaluated using an eight
828 layer Parafilm M[®] to mimic the skin insertion [74-75]. The average thickness of the
829 Parafilm layer was 127 μm and the percentage of holes created in each layer was
830 calculated using an optical microscope. An average force of 40 N was applied to each
831 MN array for 30 sec and all the MNs perforated the first three layers of the Parafilm.
832 The coated MNs perforated the fifth layer but with a lower percentage of holes (20-
833 25%), while the non-coated MNs reached the sixth layer and the percentage of holes
834 created was up to 22% (Figure S2). All the MNs successfully penetrated the third layer
835 of the Parafilm which corresponds to a penetration depth of 381 μm , indicating that
836 they can reach the skin dermis [76]. The profiles of force versus displacement of F2 and
837 F4 are depicted in Figure S3. The two coated MNs present the same mechanical
838 behavior with a continuous and gradual increase in force, suggesting that they do not
839 deform during insertion. The insertion studies suggest that the MNs subjected to EDHA
840 are capable of transdermal drug delivery.

841

842 **4. Conclusion**

843 This study demonstrated the effects of different polymeric MN coatings loaded with
844 dye. The resultant ES/ESP particular and fibrous structures were assessed and

845 characterised. Morphological studies exhibited primarily smooth fibers with some
846 beaded fibers with the PCL formulation and spherical particles. Thermal analysis
847 conferred the stability of nanoparticles and nanofibers with differential scanning
848 calorimetry also showing the dye was molecular distributed in a state throughout the
849 polymeric matrix with all 4 formulations. Spectroscopic studies also confirmed these
850 findings. As the release exponents were between 0.5 and 1, therefore the diffusional
851 release was assumed to follow anomalous transport. The drug skin permeation results
852 showed that the *in-vitro* delivery of dye in the receiver compartment after a few hours
853 was quite high. These results demonstrate that the MN shafts successfully pierced the
854 Strat-M® membrane and dissolved thus releasing a high percentage of their drug load.
855 These results show great promise for the polymers to act as a matrix for model drug.
856 However, permeation can potentially be improved with the inclusion of a permeation
857 enhancer which can enhance drug skin permeation. The application of QbD can add
858 significant value via optimisation of formulations with the most suitable permeation
859 enhancer, polymer and dye/model drug system. Thus, eliminating the need for countless
860 experiments as well as ensuring quality is built into the final product with excellent
861 release profiles and greatly enhanced permeation.

862

863

864 **References**

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1114 **Electrospinning/Electrospraying coatings for metal microneedles: a design of**
1115 **experiments (DOE) and Quality by Design (QbD) approach**

1116

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1139 **Table S1.** QTPP for fluorescein nanoparticles.

Quality Attribute	Target	Critical (Y/N)
Dosage form	Nano particles to be sprayed onto stainless steel microneedles	N
Mode of administration	Coated Microneedle	N
Route of administration	Transdermal	N
Appearance	Spherical particles	Y
Assay	95% - 105%	Y
Identity	Positive for API (fluorescein)	Y
Release profile	>75% released in 4 hours	Y
Encapsulation efficiency	>80%	Y
Particle size	< 500nm	Y
Polydispersity	< 0.3	Y

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1142 **Table S2.** QTPP for fluorescein nano-micro fibers.

Quality Attribute	Target	Critical (Y/N)
Dosage form	Nano-micro fibers to be spun onto stainless steel microneedles	N
Mode of administration	Coated Microneedle	N
Route of administration	Transdermal	N
Appearance	Smooth fibers	Y
Assay	95% - 105%	Y
Identity	Positive for API (fluorescein)	Y
Release profile	TBD	Y
Encapsulation efficiency	>80%	Y
Particle size	< 2um	Y
Polydispersity		Y

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1144 **Table S3.** QTTP for Rhodamine B nanoparticles.

Product Attribute	Target	Criticality
Route of Administration	Transdermal	No
Dosage Form	Dye loaded nanoparticles sprayed onto stainless steel MN	No
Active	Rhodamine-B dye (model drug)	No
Polymeric Carrier	PCL (Polycaprolactone)	No
Solvent	DCM (Dichloromethane)	No
Release Profile	Sustained release over a minimum of 7 days	Yes
Particle Size	1 - 500 nm	Yes
Particle Shape*	0 – 10	Yes
Poly-Dispersity Index	> 85 %	Yes
Encapsulation efficiency	> 80 %	Yes
Coating Method	EHDA process	No

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1160 **Table S4.** QTTP for Rhodamine B nano-micro fibers

Product Attribute	Target	Criticality
Route of Administration	Transdermal	No
Dosage Form	Dye loaded nano-micro fibers spun onto stainless steel MN	No
Active	Rhodamine-B dye (model drug)	No
Polymeric Carrier	PCL (Polycaprolactone)	No
Solvent	DCM (Dichloromethane)	No
Release Profile	Sustained release over a minimum of 7 days	Yes
Particle Size	0.5-2 um	Yes
Particle Shape*	0 – 10	Yes
Poly-Dispersity Index	> 85 %	Yes
Encapsulation efficiency	> 80 %	Yes

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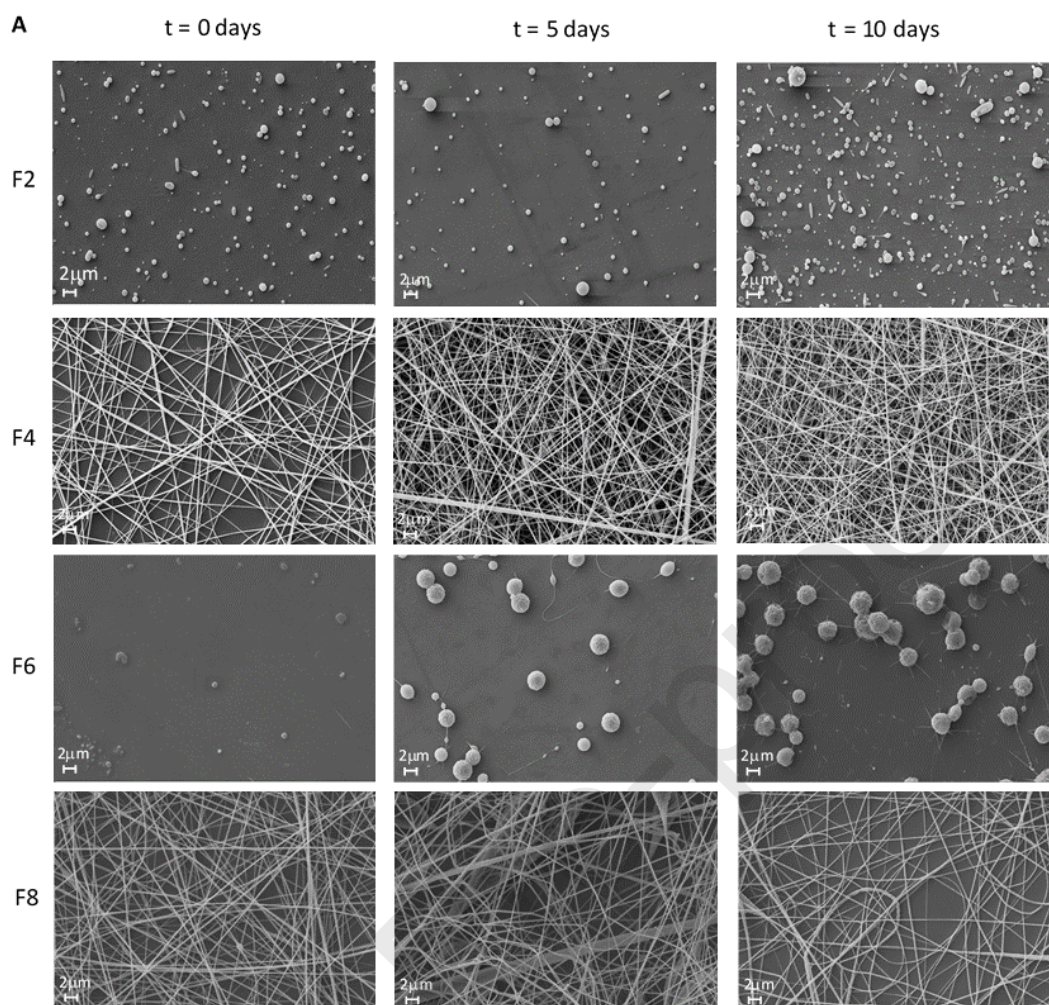
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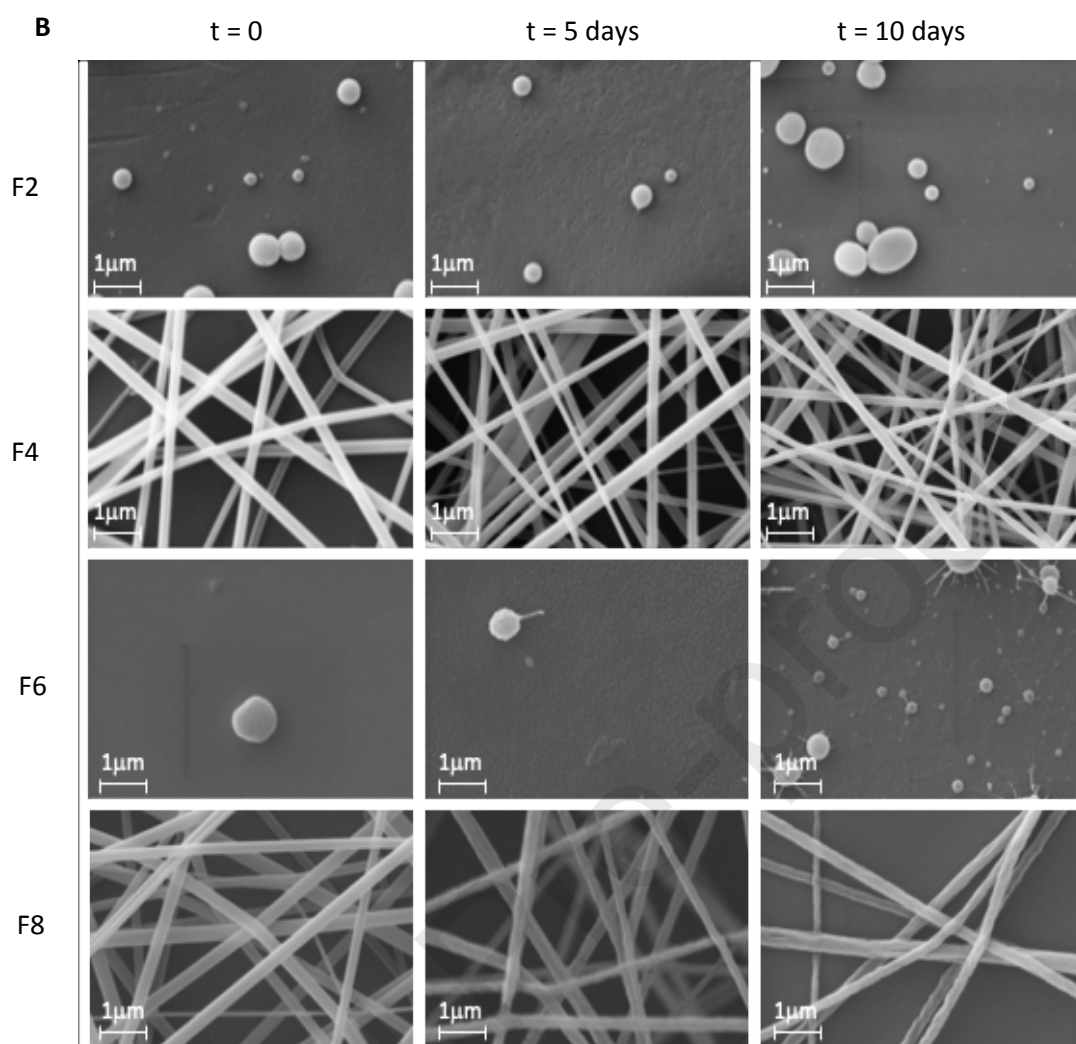
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1189 **Figure S1: SEM images showing the stability of polymeric particles and fibers over 10**
1190 **days at A) x5k magnification and B) x40k magnification.**

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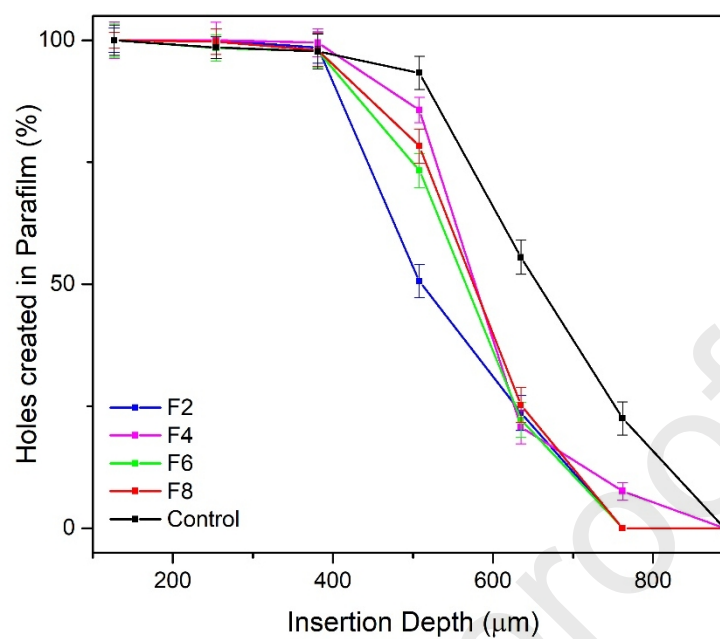
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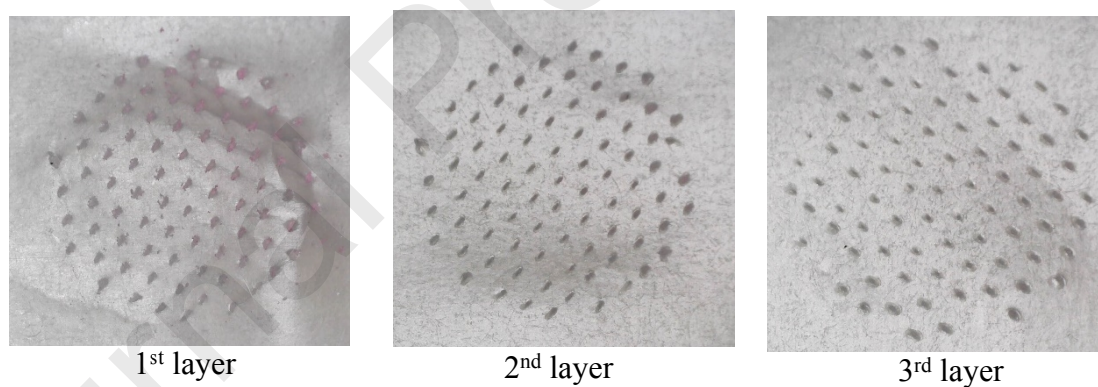
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(b)



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1201 **Figure S2. (a) Insertion of F2, F4, F6, F8 and non-coated MNs (control sample) into a**
 1202 **model membrane for skin insertion using Parafilm M[®]. (b) Photos of the first, second**
 1203 **and third Parafilm M[®] layer after insertion of F8 MNs.**

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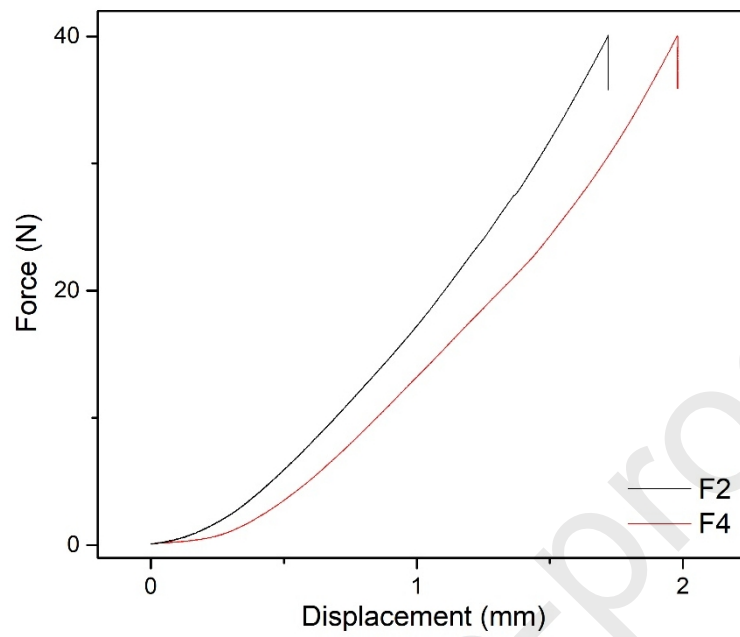
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1218 **Figure S3.** Force-displacement curves of coated MNs F2 and F4 under an axial force

1219 **load.**

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