

Platinum-catalyzed Nb-doped TiO₂ and Nb-doped TiO₂
nanotubes for hydrogen generation in proton exchange membrane
water electrolyzers

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ABSTRACT

This paper studies the catalytic activity of Pt deposited onto Nb-doped titania supports toward the hydrogen evolution reaction (HER). New catalysts based on Nb-doped TiO₂ nanoparticles (*n*Nb-TiO₂) and Nb-doped TiO₂ nanotubes (*n*Nb-TNTs), with *n* in the range 3-10 at % (Nb+Ti), were synthesized. The specific surface areas of *n*Nb-TNTs were 250–300 m²g⁻¹, about three times higher than those of *n*Nb-TiO₂. X-ray diffraction showed the Nb incorporation into the TiO₂ lattice with its consequent lattice expansion. The X-ray photoelectron spectra of Pt deposited onto Nb-doped titania revealed a negative charge accumulation on Pt, thus denoting strong metal-support interaction. The electrochemical characterization in acidic media showed that Pt supported on *n*Nb-TiO₂ and *n*Nb-TNTs presented better activity towards the HER than that of Pt deposited onto the un-doped supports and commercial Pt on carbon. The best performance was obtained with a small Nb doping of 3 at %.

Keywords: Hydrogen evolution reaction; TiO₂ supports; TiO₂ nanotubes; Nb doping; Pt catalyst; PEMWE.

1. Introduction

Within the last years, there is a renewed interest in the H₂ production from polymer electrolyte membrane water electrolyzers (PEMWEs). It is considered to be one of the most promising forms to produce high purity and fossil-free H₂ from renewable energy sources [1-5]. The most effective electrocatalysts for the hydrogen evolution reaction (HER) have been proven to be those based on Pt. However, the high cost and scarcity of Pt are a drawback in the development of large-scale applications [6]. For this reason, reducing the amount of Pt and developing Pt-free catalysts have been examined [2-13]. However, performance, corrosion resistance, mechanical stability and durability, as long as reducing the cost, are essential for the technical electrodes in PEMWEs.

The Pt loading could be reduced by improving the catalyst dispersion on high specific surface area supports and/or developing Pt-based alloys. Among the Pt-free catalysts, MoS_x- and Pd-based nanocarbons have shown reasonable good electroactivity and stability [3]. Using high specific surface area supports alternative to carbon is particularly interesting, because it allows avoiding the drawbacks associated to the use of carbon in terms of durability and performance. The H₂ and O₂ permeation between cathode and anode through the membranes of the PEMWEs has been demonstrated [14-16] and although O₂ permeation is slower than that of H₂, it increases with current density and temperature (as H₂ permeation does). The O₂ content in the H₂ product was found to be 3-4 times greater when using Pt-free instead of Pt cathode catalysts [15]. It has also been reported that the presence of O₂ at the cathode can lead to the formation of hydrogen peroxide and hydroxyl radicals, which can produce membrane and carbon degradation especially when turning off [16]. Therefore, it is interesting to explore non-carbonaceous supports with high specific surface area.

It is well known that TiO₂ has very good chemical resistance and thermal stability and has been widely investigated for different applications such as in photocatalysis and sensors [17-22]. It has also been investigated as support for Pd [23] and Pt catalysts in fuel cells [24-27] and its higher durability and stability in comparison to the conventional carbon support have been proved. Shim et al [24] studied the electrochemical performance of Pt-TiO₂/C toward the hydrogen oxidation and to the oxygen reduction in fuel cells. They explained the better performance with respect to Pt/C by an electrochemical active surface area (ECSA) increase and a lower adsorption strength of hydrogen and oxygen onto the Pt of Pt-TiO₂. Xiong and Manthiram [25], in a direct methanol fuel cell, assigned the enhanced catalytic activity of Pt/TiO₂/C toward the oxygen reduction to the increased ECSA and modified surface electronic properties of Pt. Gustavsson et al [26] attributed the better catalytic activity of Pt/TiO₂ toward the oxygen reduction reaction in comparison to Pt-black, to the better dispersion of Pt onto the oxide surface and to the substantial proton conduction of TiO₂ when a thin layer of the latter was placed between the Nafion membrane and Pt. Lewera et al [27] reported, from X-ray photoelectron spectroscopy (XPS) analyses, changes in the electronic properties of Pt deposited on a TiO₂/C composite with respect to Pt/C, induced by a strong metal-support interaction (SMSI), which was explained by the formation of a surface Pt-Ti alloy and/or a partial charge transfer from TiO₂ to Pt. This partial charge transfer would explain the reported enhanced electrocatalytic activity toward the oxygen reduction in the fuel cell cathode.

The TiO₂ conductivity is low [1,17,28,29]. However, with Nb doping, its conductivity increases by three orders of magnitude [29]. The ionic radii of Nb⁵⁺ and of Ti⁴⁺ have approximately the same size, 0.70 and 0.68 Å, respectively, thus allowing obtaining a solid solution of the former in TiO₂ [30-34]. The conductivity increase is explained by

the effect of Nb ions in providing electrons with energy levels in the TiO₂ bandgap that can be excited to the conduction band [35]. Nb-doped TiO₂ has also been satisfactorily tested as support for Pt in proton exchange membrane fuel cells (PEMFCs) [30,33,34,36,37]. Apart from increasing the TiO₂ conductivity, Nb doping allowed obtaining Nb-TiO₂ supports with greater specific surface area than that of TiO₂, thus allowing a better catalyst dispersion. Thus, Gojković et al [34] claimed that Pt/Nb-TiO₂ were promising high area supports for PEMFC anodes. Chhina et al [30] and Chevallier et al [37] found better stability for the Pt/Nb-TiO₂ catalysts than for Pt/C despite the later gave initially slight better performance. Elezović et al [33] tested the Pt/Nb-TiO₂ nanocatalyst for the oxygen reduction, finding a higher activity and methanol tolerance than Pt/C. Similar results for the oxygen reduction were found for Do et al [36]. For these supports, specific surface areas in the range from 72 [33,34] to 150 m² g⁻¹ [37] were reported.

On the other hand, Nb-doped TiO₂ supports for IrO₂ toward the oxygen evolution reaction in PEMWEs have been developed with satisfactory results [29,38,39]. Hu et al [38] prepared by means a sol-gel process a corrosion-resistant Nb_{0.05}Ti_{0.95}O₂ support of 83 m² g⁻¹. Hao et al [29] obtained mesoporous Nb(5-20 at %)-doped TiO₂ with surface areas up to 146.5 m² g⁻¹ by means of the modified evaporation-induced self-assembly method. Recently, we have prepared titania nanotubes (TNTs) doped with 3 at % Nb (3Nb-TNTs) with a surface area of 260 m² g⁻¹ [39], which is comparable to that of Vulcan XC72 of about 250 m² g⁻¹. It was found that the oxygen evolution reaction activity after supporting IrO₂ and IrRuOx increased with Nb doping [29,39]. This was explained by the surface area increase with respect to that of pristine titania, which allowed a good catalyst dispersion and accessibility, and to the ability in transferring charge of the niobium oxide

species. The stability of the Nb-doped TiO₂-supports was also shown to be better than that of unsupported IrO₂ [29].

The Pt/TiO₂ catalyst for the HER has been scarcely studied in the literature, although with promising results [40]. Thus, Pt nanoparticles supported on nitrogen-doped black TiO₂ (Pt/N_x:TiO_{2-x}) showed robust durability and onset potentials for the HER, which were somewhat smaller than that of commercial Pt/C catalyst. To the best of authors' knowledge, Nb-doped TiO₂ and TNTs have not yet been reported to be used as Pt supports for the HER. There are, however, a number of recent papers dealing with the use of Pt-free catalysts supported on TiO₂ for the HER in both, acidic [41-49] and alkaline [49-53] electrolytes. Different catalysts such as quantum dots, IrO₂ and MoS_x, Ni, Ru and Co species, were supported on nanostructured and mesoporous TiO₂ [46-49,51-53] and on TNT arrays produced by Ti anodizing [41-45,50]. The TiO₂ used was generally non-doped, although a fast electron transfer was reported for N-doped TNTs [44]. The stability results were good, although the electroactivity of such Pt-free catalysts were generally still lower than that of Pt/C. It is worth to note the exception of the porous Pd-CN_x composite [54], which needed an overpotential of only -0.055 V to reach 10 mA cm⁻², in front of a value of -0.058 V for commercial Pt/C.

Considering all the points discussed above, i.e. carbon degradation and good performance of Nb-doped TiO₂ as the anode catalyst support both, for the oxygen evolution in PEMWEs and for the H₂ oxidation in PEMFCs, it is justified studying Pt supported on Nb-doped TiO₂ and TNTs as catalysts for the HER in PEMWEs. In this paper, different Pt catalysts supported on TiO₂ and Nb-doped TiO₂, TNTs, and Nb-doped TNTs were synthesized and tested for the HER in acidic media. Nb-doped TiO₂ and TNTs were prepared by the sol-gel and modified hydrothermal techniques, respectively. Different Nb concentrations in the range 0-10 at % toward the overall amount of Nb+Ti

in TiO₂ and TNTs were investigated. Their morphological, textural and compositional properties were determined using scanning electron microscopy (SEM), transmission electron microscopy (TEM), N₂ adsorption/desorption isotherms, X-ray diffraction (XRD), XPS, and their electrochemical performance by means of cyclic voltammetry (CV) and linear sweep voltammetry (LSV). The catalytic performance of such electrocatalysts toward the HER was compared to previous results in the literature.

2. Experimental

2.1. Synthesis of the supports and Pt electrocatalysts

All reactants used in the synthesis of materials were reagent grade. Ultrapure water ($\kappa \leq 0.054 \mu\text{S cm}^{-1}$) was obtained from Millipore System Simplicity 185.

The sol-gel technique was applied for the synthesis of TiO₂ and Nb-doped TiO₂, the latter with 3, 6, and 10 at % Nb, being respectively denoted as 3Nb-TiO₂, 6Nb-TiO₂, and 10Nb-TiO₂. Titanium (IV) n-butoxide (98 %, Alfa Aesar) and niobium (V) ethoxide (99.999 %, Alfa Aesar) were mixed in absolute ethanol media (0.20 mol dm⁻³ in Nb ethoxide) in the appropriate stoichiometric ratio. Then, hydrochloric acid (37 %, Scharlau), 1 mol HCl per mol of Ti+Nb, and ultrapure water, 50 mol water per mol of Ti+Nb, were added to the mixture, vigorously stirring at room temperature for 1 h. Then, the gellification of the sol was produced by the addition of aqueous solution of 1.0 M (NH₄)₂CO₃ [31,32]. The final product was filtered, rinsed and dried at 60 °C for 10 h and afterwards, it was calcined at 350 °C in air atmosphere for 2.5 h [55].

A modified hydrothermal technique based on those previously reported in the literature for TNTs [23,55-57] and Nb-doped materials [58,59] was applied for the synthesis of the TNTs and Nb-doped TNTs. The doping concentration of Nb was 3, 6, and 10 at %, being respectively denoted as 3Nb-TNTs, 6Nb-TNTs, and 10Nb-TNTs. The amount of 1 g of

the synthesized TiO₂ or Nb-doped TiO₂ was dispersed in 100 mL of 10.0 M NaOH and placed in a Teflon[®] autoclave. The mixture was sonicated for 2 h and then, it was heated for 72 h at 130 °C [60]. The (Nb-doped) sodium titanates (Na₂Ti_xO_{2x+1}) thus obtained were protonated with 0.1 M HCl [61,62], which were rinsed with ultrapure water and dried at 60 °C for 10 h. Finally, the calcination of the (Nb-doped) protonated titanates (H₂Ti_xO_{2x+1}) at 350 °C for 2.5 h allowed obtaining the TNTs and Nb-doped TNTs.

Pt nanoparticles were dispersed on the indicated supporting materials by means of the conventional electroless deposition method, using NaBH₄ as reducing agent and sodium citrate as stabilizing agent [63]. The appropriate amount of support was dispersed in ultrapure water, followed by the addition of H₂PtCl₆·6H₂O (99.9 % metal basis, Alfa Aesar) to achieve a loading of 20 wt. % Pt in the final solid, and sodium citrate (Sigma Aldrich). The suspension was neutralized to pH 7.0 and stirred for 10 h at 50 °C before adding the NaBH₄ (Sigma Aldrich). Finally, the suspension was filtered, rinsed with ultrapure water and dried at 60 °C until constant weight. The resulting catalysts were then Pt/*n*Nb-TiO₂ and Pt/*n*Nb-TNT, *n* indicating the Nb content (with values of 0, 3, 6 and 10 at %). It has been reported that the Nb-doped TiO₂ catalysts have conductivities about 10³ S cm⁻¹ and that they increase with Nb doping [29], which is small compared to those reported for Vulcan carbon XC72 and XC72R of 4.5 [64] and 2.8 S cm⁻¹ [65], respectively. However, the Pt deposition can significantly change the conductivity of the sample, as previously shown when the conductive IrO₂ was deposited on Nb-doped TiO₂ [29]. In this case, the conductivity of the latter was increased in this form by one or two orders of magnitude. Commercial 20 wt. % Pt on Vulcan XC72 catalyst (Pt/C) from Premetek was taken as a reference for comparison purposes.

2.2. Physicochemical characterization of the supports and catalysts

The SEM images of the titania supports were taken using a JSM5910-LV JEOL microscope. The Nb:Ti atomic ratios of the supports and the mass ratio of the metal to the support in the electrocatalysts was analyzed by the energy dispersive X-ray (EDX) technique, using an INCA-300 energy analyzer coupled to the scanning electron microscope.

The catalysts were examined by TEM, using a JEOL JEM-1400PLUS microscope, equipped with a GATAN US1000 CCD camera (2k×2k) and operating at 120 kV. Prior to the observation, the specimens were dispersed and sonicated for 10 min in ethanol, and then deposited onto a carbon-coated copper grid.

The textural properties of the supports were determined by N₂ adsorption/desorption isotherms at 77 K, using a Micromeritics ASAP 2020 instrumentation, after outgassing for 10 hours at 150 °C under vacuum (10⁻⁵ torr). The specific surface area (*S*_{BET}) was determined using the Brunauer-Emmet-Teller (BET) equation and taking 0.162 nm² as the cross-sectional area of the N₂ molecule. The pore volumes and pore size distributions were obtained from the desorption branches of isotherms by means of the Barret-Joyner-Halenda (BJH) model.

The XRD patterns were obtained by a Bruker D8 Advance diffractometer operating with Cu K_α radiation ($\lambda=1.5406 \text{ \AA}$) and a 2θ scan from 5 to 80° (at 0.01° min⁻¹). The diffraction peaks were assigned according to the International Centre for Diffraction Data (ICDD) cards in PDF-2 database. The XRD data were used to determine the lattice parameter from the interplanar distances, and the average crystallite size by using Scherrer equation [66].

The XPS experiments were performed in a SPECS Sage HR 100 spectrometer with a non-monochromatic X ray source of Magnesium with a K_α line of 1253.6 eV energy and

250 W. The selected resolution for the high-resolution spectra was 15 eV of Pass Energy and 0.15 eV step⁻¹. Measurements were made in an ultra-high vacuum (UHV) chamber at a pressure around 8×10^{-8} mbar. The samples were placed perpendicular to the analyzer axis and the internal calibration was performed using the 1s line of adventitious carbon at 284.6 eV. Asymmetric and Gaussian Lorentzian functions were used for the band deconvolution (after a Shirley background correction), constraining the full width at half maximum (FWHM) of all the peaks and setting free the peak positions and areas.

2.3. Electrode preparation and electrochemical characterization

An amount of 10 mg of the catalyst was dispersed in 0.50 mL mixture of isopropanol and ultrapure water (1:1 by volume), and sonicated for 30 min. The required amount of this suspension was placed by means of a micropipette onto the surface of a glassy carbon (GC) disk (0.0707 cm² in section) to achieve a Pt loading of 14 $\mu\text{g}_{\text{Pt}}\text{cm}^{-2}$ and dried under a slow nitrogen flow (Air Liquide, purity $\geq 99.995\%$). It was then covered with 5 μl of a 0.05 % Nafion[®] solution diluted in ethanol and dried again under nitrogen. Before each analysis, the GC disk was polished to a mirror finish using alumina powder suspensions (0.3 μm and 0.05 μm , Buehler), followed by sonication in water.

The electrochemical measurements were conducted with a potentiostat PARSTAT 2273 (Ametek, Inc.) controlled by the PowerSuite 2.58 software in a thermostatic three-electrode glass cell at 25.0 ± 0.1 °C. The cell was placed inside a Faraday cage, and the experiments were carried out under dark conditions (to avoid any possible photoelectrocatalytic effect coming from the studied materials). The working electrode was the catalyst-covered GC one and the reference electrode was the mercurous sulfate electrode (MSE) Hg|Hg₂SO₄|K₂SO₄(sat) (Radiometer Analytical). However, all the potentials reported in this work are expressed vs. the reversible hydrogen electrode (RHE). The auxiliary electrode was a Pt wire and the electrolyte was an aqueous solution

0.50 mol dm⁻³ H₂SO₄ (prepared from Merck Suprapure[®]), deaerated by N₂ bubbling through the solution for 20 min.

For the electrochemical experiments, the electrode was immersed into the N₂-purged electrolyte, and it was cycled in the potential window 0.050–1.200 V at a scan rate of 100 mV s⁻¹ until reproducible cyclic voltammograms were obtained. The Pt ECSA was estimated from the net charge for hydrogen adsorption/desorption profiles in the cyclic voltammograms recorded at scan rate 20 mV s⁻¹ under N₂ inert atmosphere, assuming that a charge of 210 μC cm⁻² was needed to produce a monolayer of adsorbed H on polycrystalline Pt [67].

The HER was studied by LSV without stirring in a cathodic sweep in the range from 0.100 to -0.100 V at a scan rate of 1 mV s⁻¹ and with ohmic-drop correction. The *IR*-drop in solution was measured using electrochemical impedance spectroscopy. The impedance spectra were obtained at the open circuit potential, in the frequency range from 100 kHz to 0.1 Hz, superposing an *ac* amplitude of 5 mV. All these *j*-*E* curves were corrected by the uncompensated resistance and repeated three times for each catalyst to test their reproducibility.

3. Results and discussion

3.1. Physicochemical characterization of the supports based on TiO₂ and TNTs

The different morphology of the TiO₂ and TNTs supports are exemplified in Figs. 1 and 2. Fig. 1a and b shows the SEM images of TiO₂ and TNTs with 3 at % Nb doping, respectively, where the different size and morphology of the constituent particles are apparent. A prismatic shape typical of TiO₂ is shown in Fig. 1a, with evident porosity, whereas the morphology of the TNTs is completely different, with randomly oriented thin

nanotubes looking like a cobweb, in which greater porosity and specific surface area are expected.

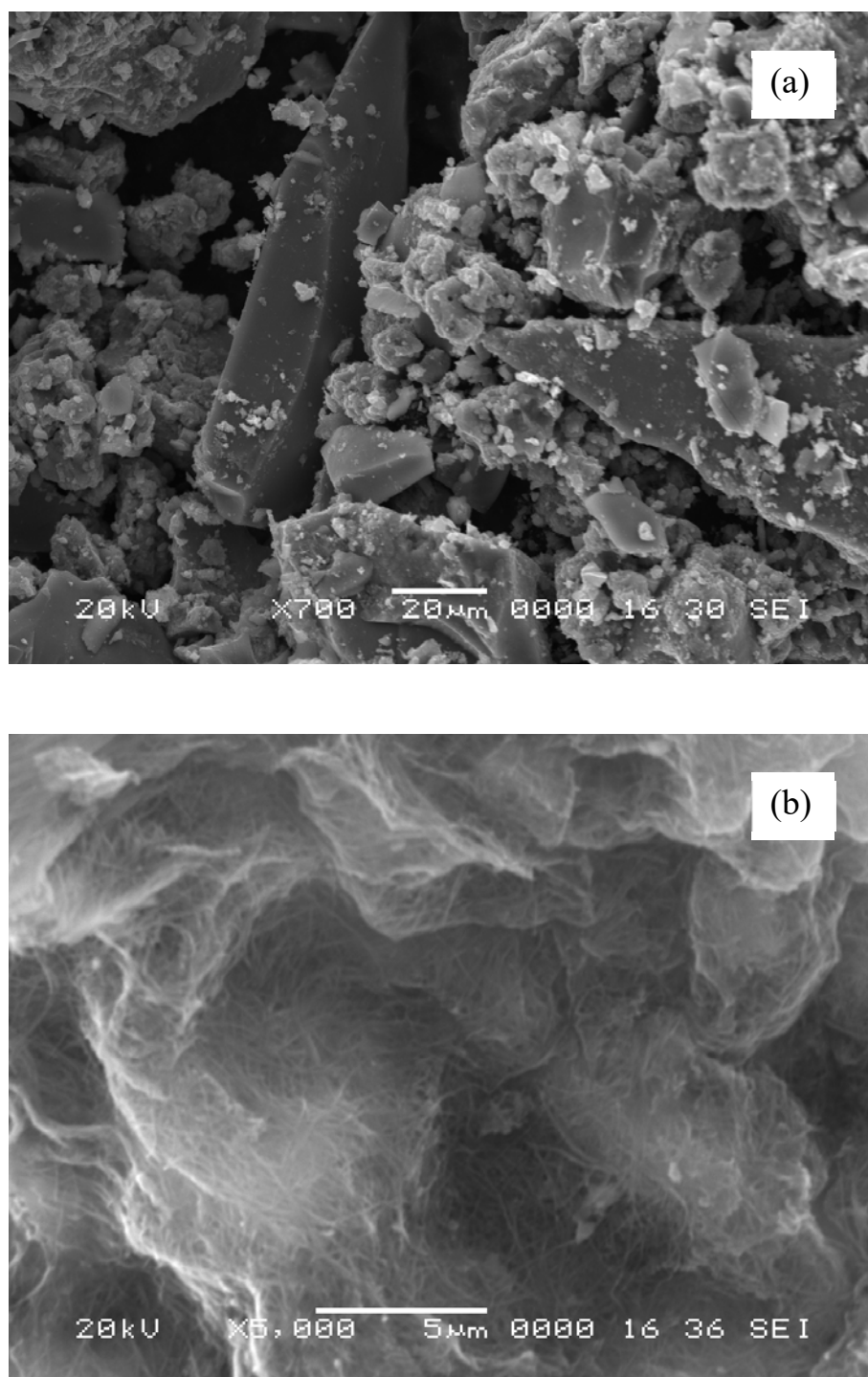
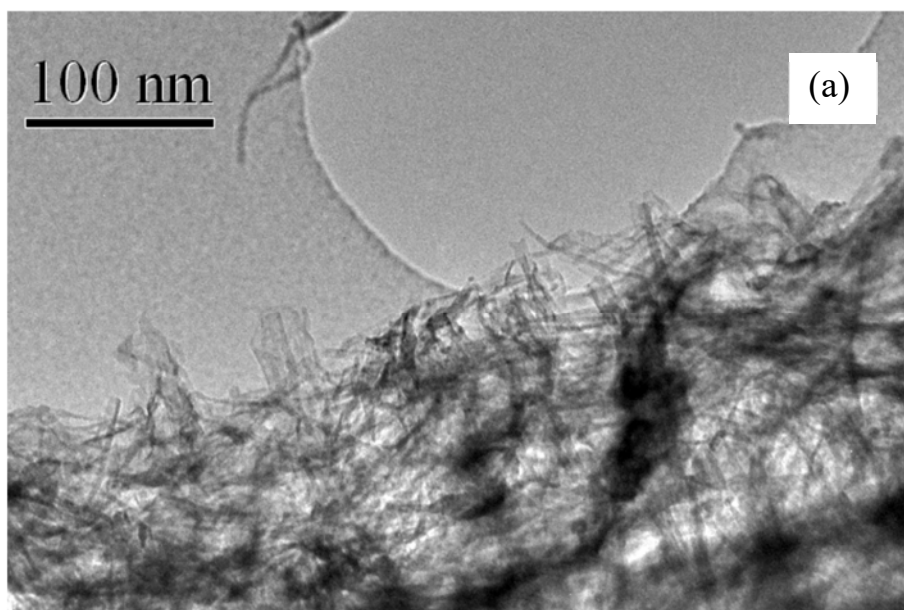


Fig. 1 – SEM images of different supports: (a) 3 Nb-TiO₂ and (b) 3Nb-TNTs.

Details at different magnifications of 3Nb-TNTs are shown in the TEM pictures of Fig. 2a and b. The TEM image of Fig. 2b shows the Nb-doped nanotubes, which were about 10 nm in the outer diameter and in the range 100-200 nm in length. A high-resolution image of the same support is given in Fig. 2c, where the end of a nanotube together with the corresponding selected area electron diffraction (SAED) are shown. The string pattern of the SAED is the expected one for a tube-shaped crystal [56] and it is in agreement with previous work showing that the nanostructures produced by hydrothermal reaction depend on different process parameters. Thus, nanotubes were obtained from TiO₂ crystals, whereas nanofibers with interlinked structure were formed from amorphous TiO₂ [68], the SAEDs of the latter presenting diffuse rings of amorphous phases.



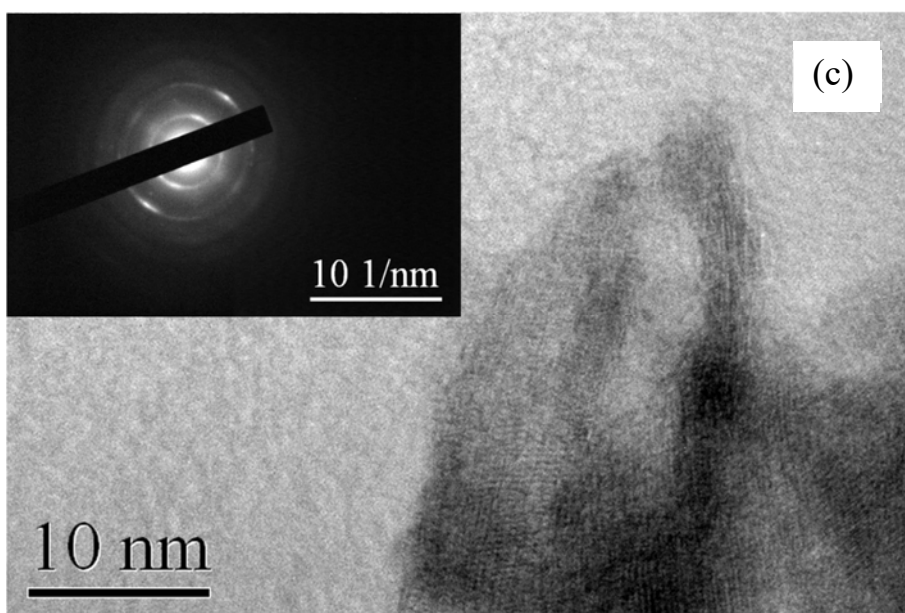
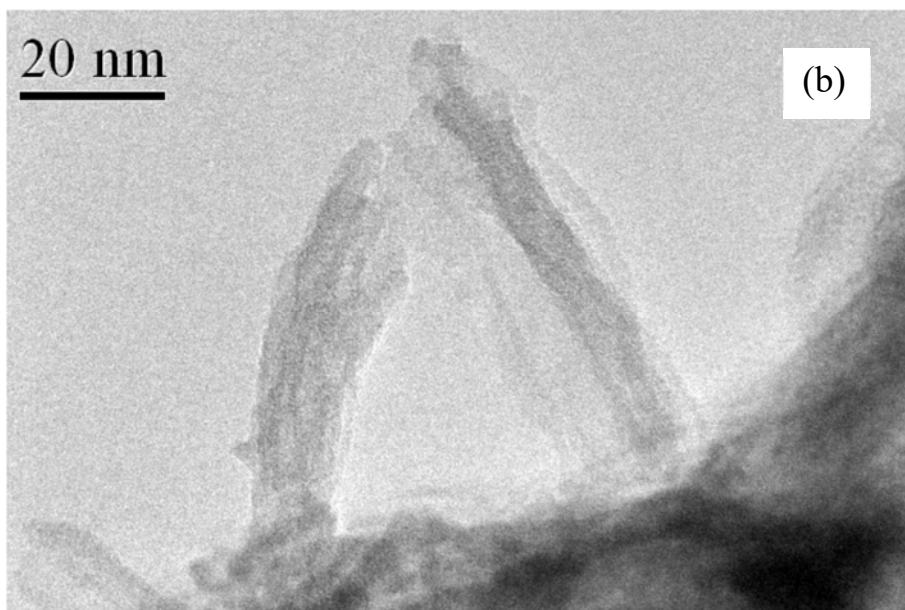


Fig. 2 – TEM pictures of 3Nb-TNTs at different magnifications: (a) general view, (b) detail of the nanotubes and (c) a high-resolution image of a nanotube with the corresponding SAED in the inset.

The textural properties of the supports studied are listed in Table 1. The specific surface areas, S_{BET} , for TiO_2 and Nb-doped TiO_2 are in the range 80-100 $\text{m}^2 \text{g}^{-1}$. As shown in this table, the surface area increased with the Nb content, although the corresponding pore diameter and volume decreased. The same trend in S_{BET} and pore diameter can be observed for TNTs doped with Nb, the specific surface areas rising from 145 to 303 $\text{m}^2 \text{g}^{-1}$, values corresponding to the undoped and to a Nb doping of 10 at %, respectively. In this case, however, the pore volume increased with the Nb content. It is worth to note that the pore volumes and diameters, together with the surface areas were about 2-3 times greater for the TNTs. These changes in the textural properties appeared to be due to the different size of the titania nano-building blocks generated during the synthesis procedure, which were packed in a different form during calcination [29,39].

Surface areas of 68 and 143 $\text{m}^2 \text{g}^{-1}$ were previously reported in the literature for mesoporous titania, without Nb doping and with 5 at % Nb, respectively, with no further significant change when Nb doping was increased to 20 at % [29]. The surface areas reached with the Nb-doped TNTs of this work were greater than previous values reported in the literature for $\text{Nb}_{0.05}\text{Ti}_{0.95}\text{O}_2$ powders (83 $\text{m}^2 \text{g}^{-1}$) [38] and mesoporous $\text{Nb}_{0.1}\text{Ti}_{0.9}\text{O}_2$ (147 $\text{m}^2 \text{g}^{-1}$) [29]. The surface areas of the Nb-doped TNTs obtained in this work were also greater than that reported for commercial Vulcan XC72 (Cabot Corp.), one of the most used carbon black as catalyst support, with a value of about 250 $\text{m}^2 \text{g}^{-1}$ [11,12,65]. Therefore, the Nb-doped TNTs appeared to be suitable for application as catalyst supports in porous diffusion electrodes. Compared to these values, the surface areas of TiO_2 were somewhat smaller and then, TNTs seem to be better candidates as catalyst supports.

The X-ray diffractograms of the supports based on TiO_2 and TNTs with different Nb contents are depicted in Fig. 3a and b, respectively. The typical peaks of the anatase phase of titania have been clearly identified for both supports. It is also shown in these figures

that when the amount of Nb increased, the anatase peaks became wider, thus suggesting smaller anatase crystallite size with Nb doping. The mean crystallite size was estimated from Scherrer's equation and the corresponding results are also listed in Table 1. It is shown that the crystallite sizes for Nb-doped TiO₂ (in the range 6.4-7.3 nm) were smaller than that for undoped TiO₂ (8.7 nm). Similar results were found for the TNTs, the values for the Nb-doped TNTs being smaller (in the range 6.5-7.8 nm) than for the undoped ones (8.8 nm). This agrees with the previously observed grain growth inhibition by the Nb dopant in titania nanopowders [32] and in Pb(ZrTi)Nb_xO₃ ($x = 0.02-0.06$) ceramics [69]. The Nb effect can then be explained in the same form. The vacancies created by Nb doping are supposed to be bound to Nb. As the grain growth involves the lattice diffusion of vacancies from pores to grain boundaries, the doping Nb ions can diminish the mobility of the vacancies and concentrate near the grain boundaries, thus resulting in smaller grain size. Note, however, that when the Nb content increased, the crystallite size also increased, although remaining under the crystallite size of the undoped titania. This may be related to the increase in the number of vacancies created with rising the Nb content, because such vacancies are needed for the grain growth.

Table 1 – Textural properties from BET analysis of N₂ adsorption, and crystallite size and lattice parameters from XRD, of the different supports studied.

Support	Nb content^a / at %	Pore volume / cm³ g⁻¹	Pore diameter / nm	S_{BET} / m² g⁻¹	Crystallite size / nm	Lattice parameter / Å
TiO ₂	0.0	0.202	7.08	80	8.7	4.9782
3Nb-TiO ₂	3.3	0.178	6.05	87	6.4	4.9860
6Nb-TiO ₂	6.2	0.165	4.87	93	6.5	4.9865
10Nb-TiO ₂	10.8	0.126	3.77	100	7.3	4.9978
TNT	0.0	0.581	13.4	145	8.8	4.9865
3Nb-TNT	3.1	0.769	9.33	260	6.5	5.0007
6Nb-TNT	6.1	0.817	9.25	278	6.9	5.0049
10Nb-TNT	11.1	0.861	9.13	303	7.8	5.0544

^a Mean standard deviation of 0.3 at %

Fig. 3a and b also shows a slight shift of the peaks toward lower angles when titania is doped with Nb, thus predicting a lattice expansion with the Nb introduction in the titania lattice. Bragg's law allowed determining these lattice parameters, which are also given in Table 1. These values clearly confirm the lattice expansion with Nb doping, the lattice parameter increasing with the Nb content due to the higher size of Nb(V) with respect to Ti(IV). These results are also consistent with previous ones reported in the literature for rutile 10Nb-TiO₂, with a greater lattice parameter than rutile TiO₂ [70].

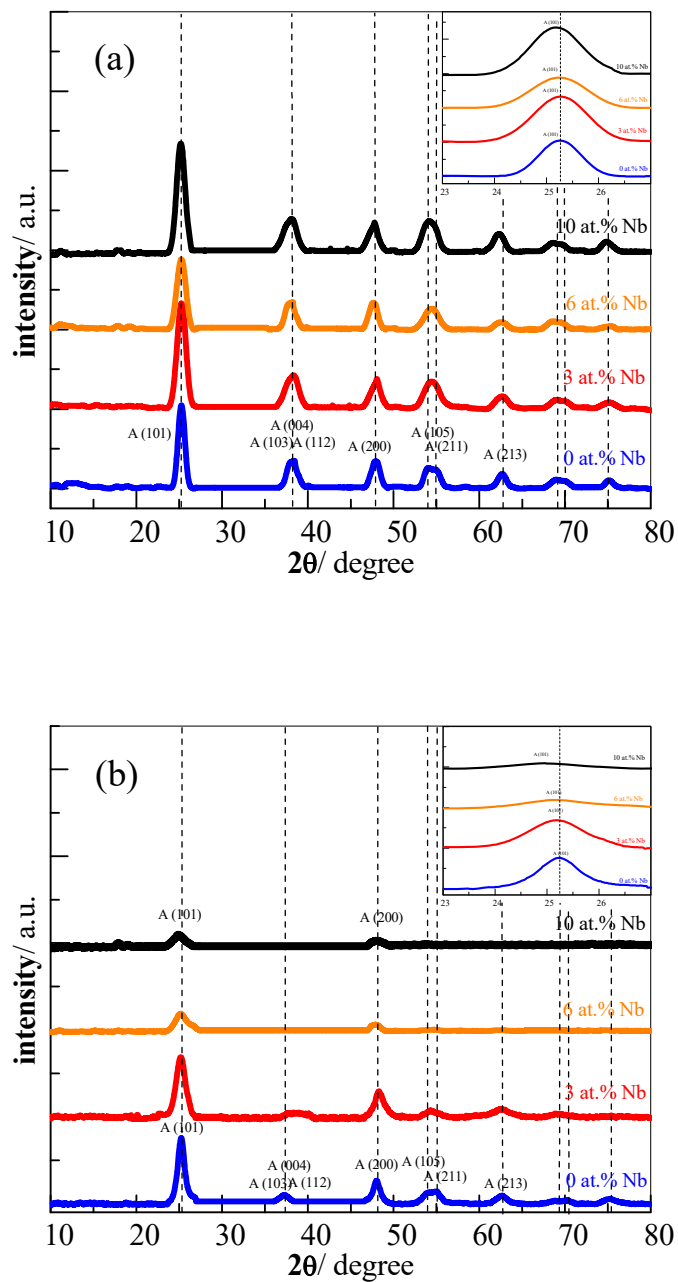


Fig. 3 – X-ray diffractograms of the supports with different Nb content: (a) TiO₂ and (b) TNTs. In parentheses, planes corresponding to characteristic diffraction signals of anatase, A. The inset is a magnification of peak A(101) to show its displacement towards smaller angles with Nb doping.

3.2. Physicochemical characterization of Pt electrocatalysts

Fig. 4 depicts selected TEM images of the 20 wt % Pt/3Nb-TNT catalyst. Fig. 4a shows that the Pt nanoparticles were homogeneously dispersed over the TNTs. Such a dispersion suggests a suitable contact between the catalyst and the support and allows providing a good electronic conductivity of the supported catalyst [71,72]. The compositional results obtained from the EDX analyses performed by SEM are given in Table 2.

Table 2 – Structural and electrochemical characteristics of Pt supported to 20 wt % on the different Nb-doped TiO₂ and TNTs.

Electrocatalyst	Pt content^a / wt %	Crystallite size / nm	Lattice parameter / Å	ECSA / m² g⁻¹
Pt/TiO ₂	20.7	4.9	3.92	12
Pt/3Nb-TiO ₂	18.8	4.1	3.92	14
Pt/6Nb-TiO ₂	19.2	4.6	3.93	11
Pt/10Nb-TiO ₂	18.1	5.2	3.92	12
Pt/TNT	19.6	4.4	3.93	14
Pt/3Nb-TNT	20.7	3.9	3.92	11
Pt/6Nb-TNT	18.8	4.9	3.92	13
Pt/10Nb-TNT	17.6	4.5	3.93	11

^a Mean standard deviation of 0.9 wt %

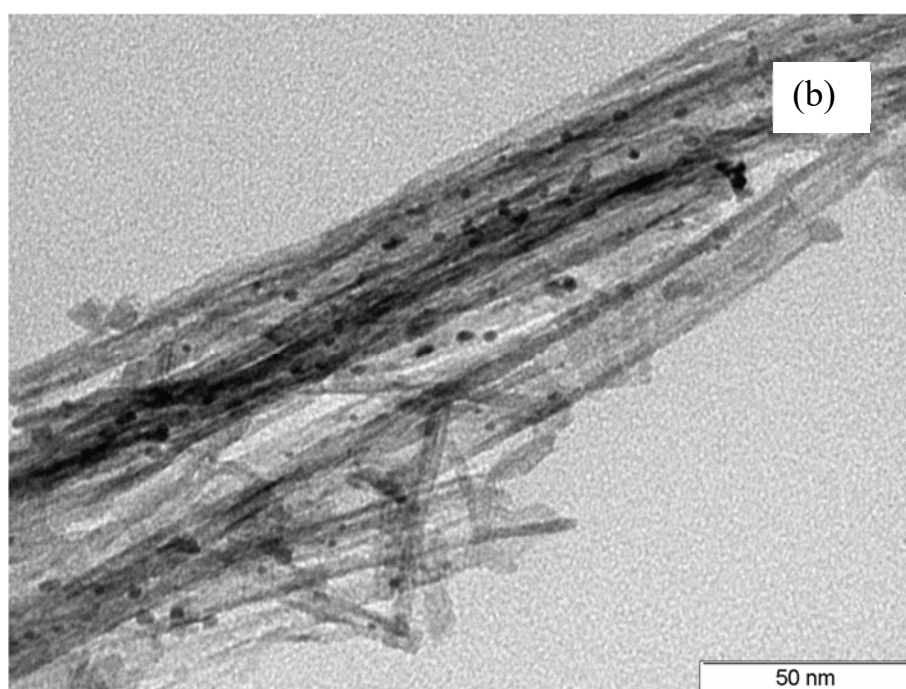
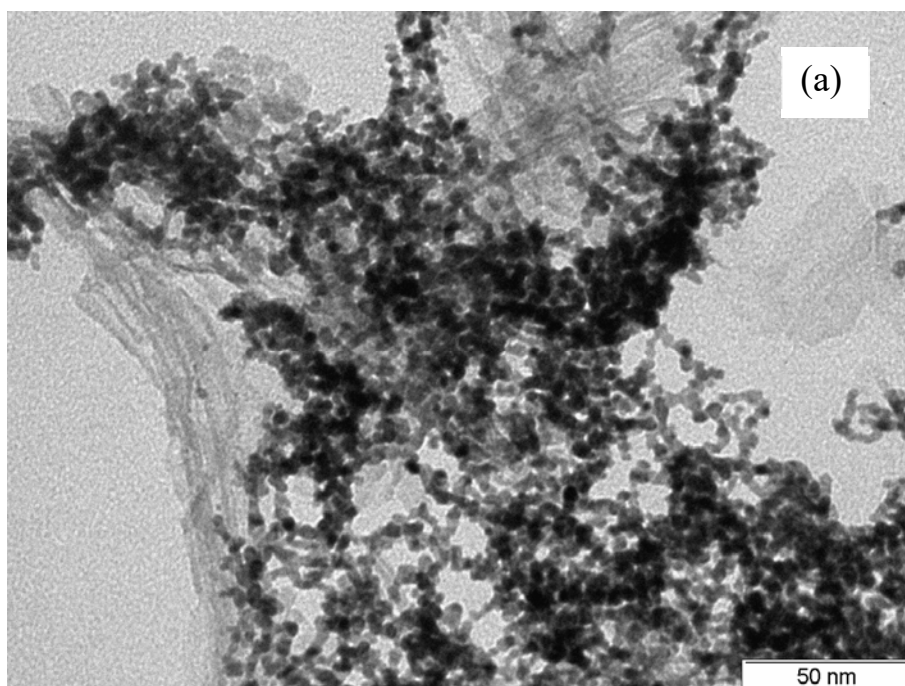


Fig. 4 – TEM pictures of 20 wt % Pt/3Nb-TNT at different magnifications: (a) general view and (b) detail of the Pt dispersion on the nanotubes.

The diffractograms corresponding to Pt supported on TiO₂ and on TNTs for different Nb contents are depicted in Figs. 5a and b, respectively. Typical peaks for (111), (200) and (220) planes, characteristic of the face-centered cubic (*fcc*) lattice structure of platinum, which appear at 2θ values of 39.7, 46.2 and 67.6, respectively, are indicated. In all cases, it is shown that Pt peaks are superimposed to the anatase ones shown in Figs. 3a and b. From Scherrer equation and Bragg's law, the corresponding crystallite sizes and lattice parameters were obtained (see Table 2). The lattice parameters were always found to be close to $a = 3.922 \text{ \AA}$, confirming that the nanoparticles consisted of pure Pt. The crystallite sizes, estimated from the (111) Pt peak, are also listed in Table 2. Values in the range 4.1-5.2 \AA were obtained for the Pt nanoparticles supported on TiO₂, whereas they were in the range 3.9-4.9 \AA for TNTs. This difference is small, but it seems that there is some dependence on the support. With 3 at % of Nb doping, the Pt crystallite size is smaller than that on the non-doped titania (TiO₂ and TNTs). However, it increases with further additional Nb doping. The smaller crystallite size of Pt for 3Nb-TiO₂ and 3Nb-TNT can be explained by the nucleation at more sites of the later supports with respect to TiO₂ and TNTs due to an increase in the surface area (Table 1). The increase in the crystallite size of Pt with further Nb doping does not match with the corresponding increase in the BET surface area. This appears to be related to the pore diameter, since according to Table 1, it decreases when the Nb content increases and then, the surface area increase is probably less effective in providing more nucleation sites. This is more marked in the case of the TiO₂ supports, which have smaller pore diameters than those of TNTs and consequently, the corresponding Pt crystallite sizes on the former are somewhat greater.

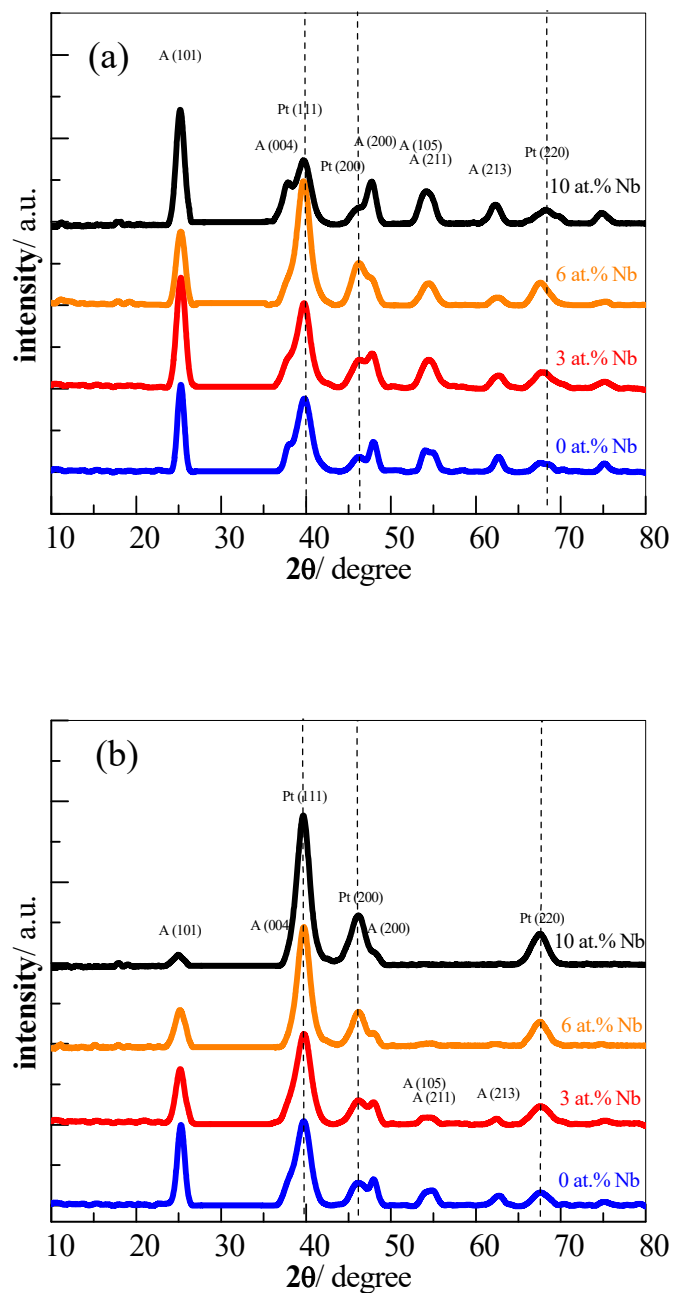


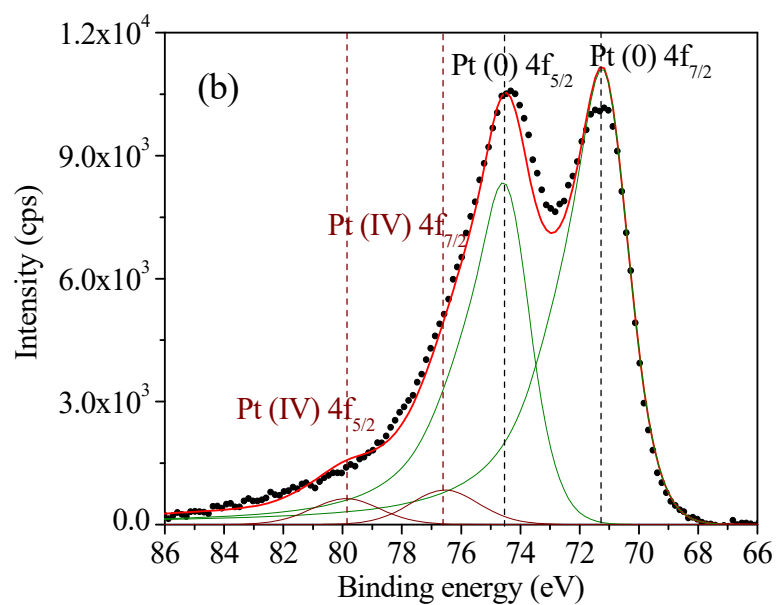
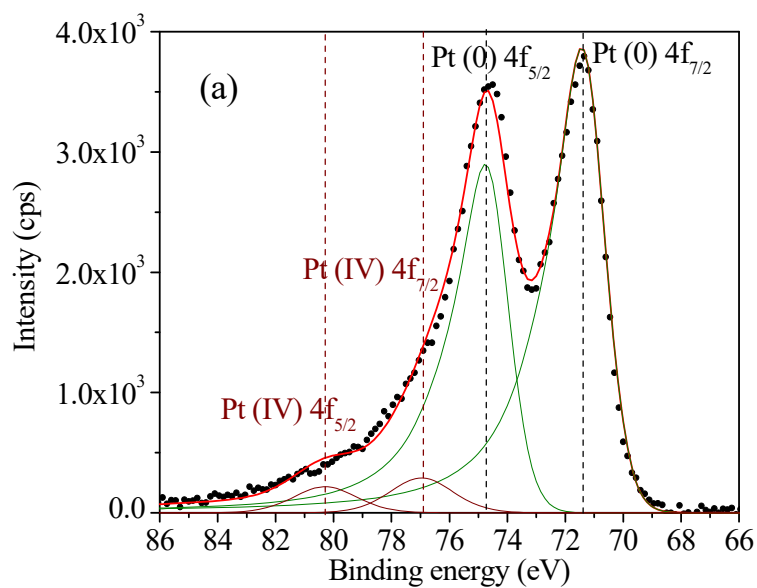
Fig. 5 – X-ray diffractograms of Pt supported to 20 wt % on (a) TiO₂ and (b) TNTs, with the indicated Nb contents. In parentheses, planes corresponding to characteristic diffraction signals of anatase, A, and *fcc* Pt.

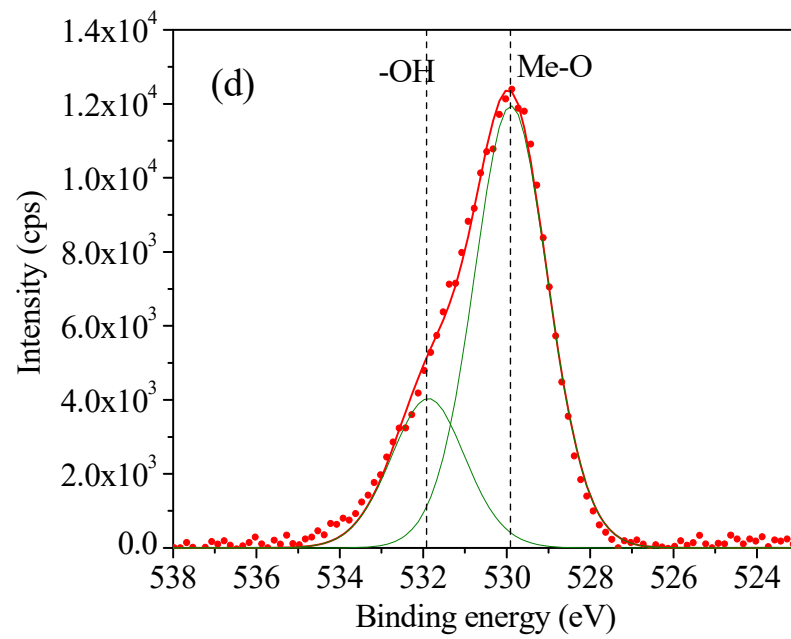
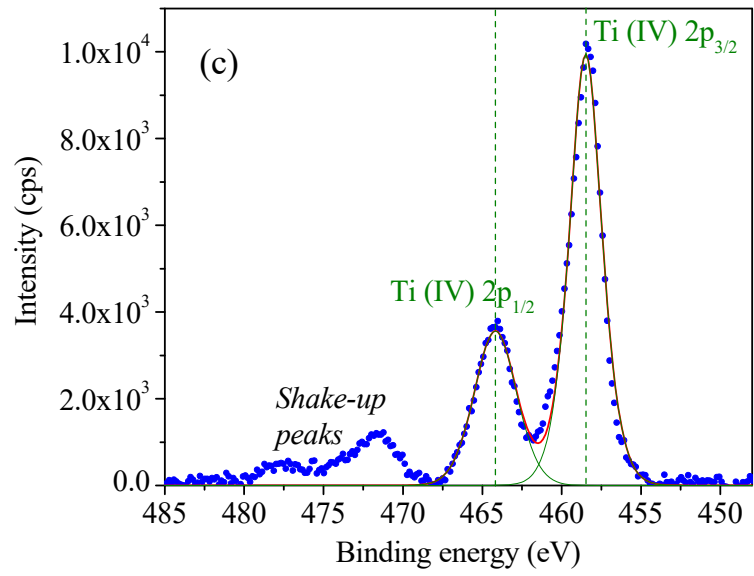
Fig. 6a and b shows the Pt 4f XPS spectra of 20 wt % Pt/C and of 20 wt % Pt/3Nb-TNT, respectively. As shown in Fig. 6a, the main Pt 4f_{7/2} and Pt 4f_{5/2} peaks of 20 wt % Pt/C are located at about 71.43 and 74.73 eV, and can be mainly assigned to Pt(0) [73]. Similar results have been obtained for 20 wt % Pt/3Nb-TNT, with the respective Pt 4f_{7/2} and Pt 4f_{5/2} peaks located at about 71.31 and 74.61 eV, which can also be assigned to Pt(0) [73]. There is a shift of the Pt 4f signal of about 0.12 eV for Pt/3Nb-TNT to lower binding energies in comparison to the Pt/C reference catalyst. This difference suggests a local increase of the electron density on Pt in the former with respect to the later, thus suggesting a SMSI between Pt and the support in Pt/3Nb-TNT, comparable to that previously claimed for Pt-TiO₂ [24-27], which favored the kinetics of the oxygen reduction reaction, due to such a positive effect of the substrate.

With regard to the peaks deconvolution, also shown in Figs. 6a and b, the Pt(0) and Pt(IV) signals have been considered. Note that the Pt(0) component was fitted to an asymmetric shape, which is characteristic of conductive materials. The deconvolutions depicted in Figs. 6a and b clearly show that the main contributions are due to Pt(0). The Pt(IV) ones are minor and the Pt 4f_{7/2} peaks of 20 wt % Pt/3Nb-TNT and 20 wt % Pt/C are located at about 76.57 and 77.00 eV, respectively, the bonding energy shift being also in agreement with the different chemical nature of both supports.

The binding energy regions of Ti, O and Nb for 20 wt % Pt/3Nb-TNT are depicted in Figs. 6c, d and e, respectively. In Fig. 6c, the main Ti 2p_{3/2} peak is located at about 458.5 eV, which corresponds to Ti(IV), bond with oxygen in TiO₂ [29,39]. The characteristic shake-up peaks of TiO₂ are also observed and shown in the figure. We tried the deconvolution of the Ti peaks considering the possibility of Ti(III), with binding energies of 457.8 and 463.2 eV [29], but no convincing results were obtained and therefore, if present, it would be in a very small amount. It is also worth to mention that in a previous

work of the authors using the same supports with Ir-based catalysts [39], the smaller binding energy of Ti(IV) in TNTs was 458.8, but changed to 458.4 eV in 3Nb-TNTs, value which is close to that found in this paper. This means that the electronic state of Ti was slightly modified from pure Ti(IV) when going from TNTs to 3Nb-TNTs.





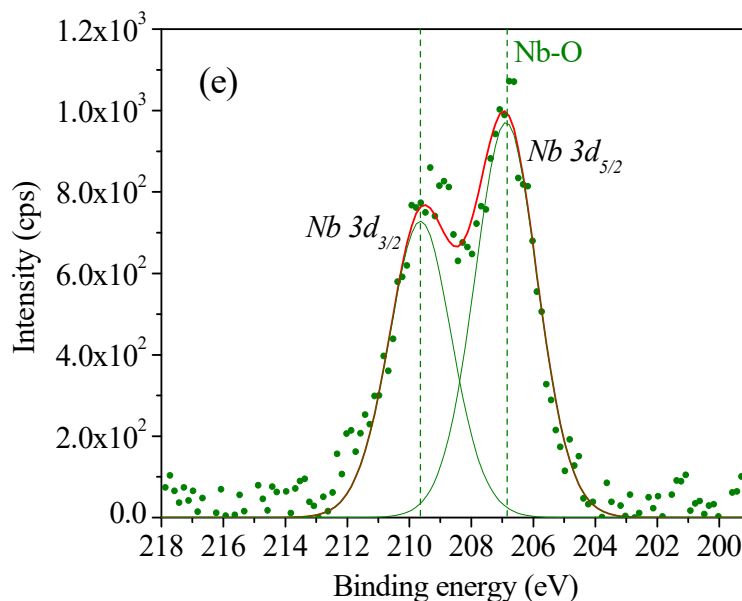


Fig. 6 – High-resolution XPS spectra in the different binding energy regions of (a) Pt 4f for 20 wt. % Pt/C and (b) Pt 4f, (c) Ti 2p, (d) O 1s and (e) Nb 3d for 20 wt % Pt/3 Nb-TNT.

Fitting of the O1s binding energy profile revealed the presence of two components (see Fig. 6d), the main one at around 529.9 eV, which could be attributed to oxygen from the Nb-TNTs. This one appears at a somewhat smaller BE than that of 530.6 eV reported for oxygen from TiO₂ [27], but this could be due to the different support composition. On the other hand, the smaller BE peak at around 531.9 eV could be due to surface -OH groups, oxygen species on carbon and carbonate species, which can be expected on the surface of this kind of supports. The same value of 531.9 eV was assigned for all present oxygen-containing species on carbon and Pt, including Pt oxides on Pt/C [27]. In our case, the presence of Pt(IV) oxide is not probable because the Pt(II) signal is missing and the small Pt(IV) signal appears at 76.5-77.0 eV instead of at 74.2 eV [74], thus indicating that the former is probably related to the cation bonding to very electronegative species such as chloride.

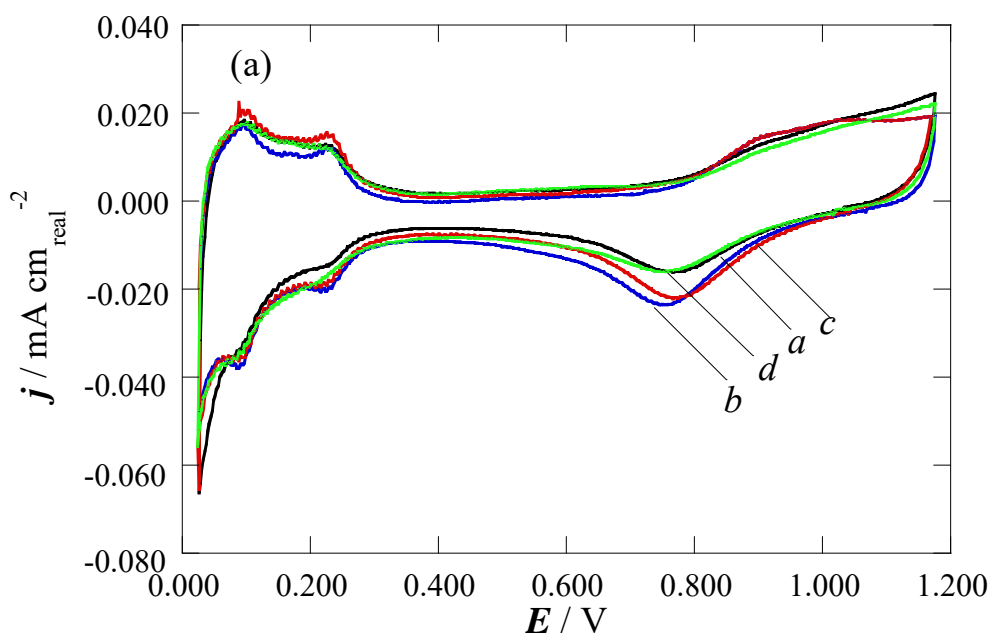
On the other hand, Fig. 6e shows that the main Nb 3d_{5/2} binding energy peak is located at around 206.8 eV, which can be attributed to the Nb-O bonds in NbO₂ [29,39,73]. This value is somewhat higher than that one of 206.0 eV reported previously in the literature for Nb(IV) [29]. For this reason, we also tried the deconvolution of the Nb peaks considering the Nb(V) species, with binding energies of 207.5 and 210.2 eV [29], but this was not feasible. However, it is interesting to note that the Nb(IV) peaks in Fig. 6e slightly tended to Nb(V) (i.e. to higher BEs) whereas the Ti(IV) peaks of Fig. 6c slightly tended to Ti(III) (i.e. to lower BEs). This suggests some electronic modification in both, Ti and Nb in 3Nb-TNTs, which can be explained considering that this low valence state of Nb in the oxide can generate an electron donor level in the forbidden region of the titania bandgap. The shift of the O1s peak to a smaller BE of Fig. 6d when compared to that from TiO₂ [27] is also in agreement with the electron donor characteristics of Nb. This would lead to free electrons in the conduction band of titania, which would increase the conductivity of the support [75].

3.3. Electrochemical characterization of the Pt electrocatalysts

Control CV experiments in deaerated 0.50 mol dm⁻³ H₂SO₄ were first performed to analyze the *j*-*E* profile of the Pt nanoparticles deposited on the different supports. Fig. 7a and b shows the cyclic voltammograms corresponding to Pt supported on TiO₂ and TNTs, respectively, after normalizing with respect to the ECSAs (see Table 2). These were determined from the ratio between the charge associated to the hydrogen adsorption/desorption peaks of the cyclic voltammograms and the Pt load ($\mu\text{C } \mu\text{g}_{\text{Pt}}^{-1}$), divided by a charge of 210 $\mu\text{C cm}^{-2}$ for a monolayer formation of adsorbed hydrogen on polycrystalline Pt [76]. The real current densities plotted in Fig. 7a and b were then obtained by dividing the specific current densities ($\text{mA } \mu\text{g}_{\text{Pt}}^{-1}$) by the corresponding ECSAs.

The values of the ECSAs varied in the range 11–14 $\text{m}^2 \text{g}_{\text{Pt}}^{-1}$ (see Table 2), that is without significant differences for the two types of supports used. The results listed in Table 2 indicate that comparable nanoparticle size, dispersion and aggregation were obtained by means of the electroless deposition of Pt, performed under the same conditions, on the different supports studied. Note that these values were smaller than that determined for commercial Pt/C, which was of 43 $\text{m}^2 \text{g}_{\text{Pt}}^{-1}$, due to its smaller nanoparticle size. The j – E profile normalized by the ECSA corresponding to Pt/C is depicted in curve *i* of Fig. 7c. It is shown in Fig. 7c that the normalized j – E profiles of Pt supported on TiO_2 (curve *j*) and TNTs (curve *k*) match very well with that of commercial Pt/C.

Fig. 7a and b shows the typical features of polycrystalline Pt for all the supported catalysts studied [77], thus indicating good Pt-support interaction. The peaks corresponding to hydrogen adsorption/desorption, in the potential range 0.03–0.30 V, are well resolved. The Pt oxidation started at about 0.75 V and the cathodic peak potential at about the same potential corresponded to the Pt oxide reduction.



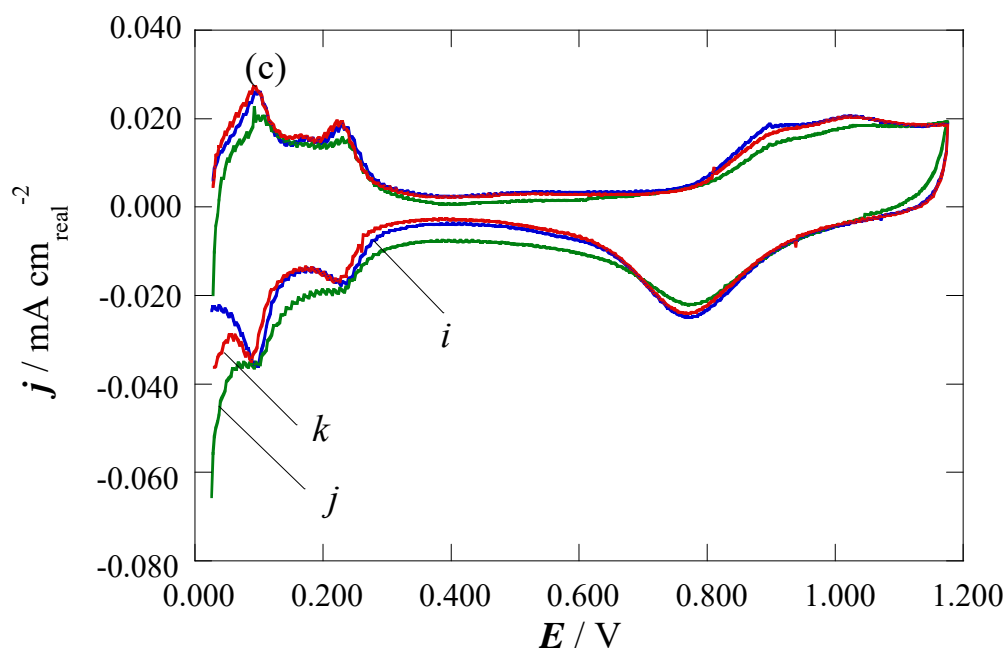
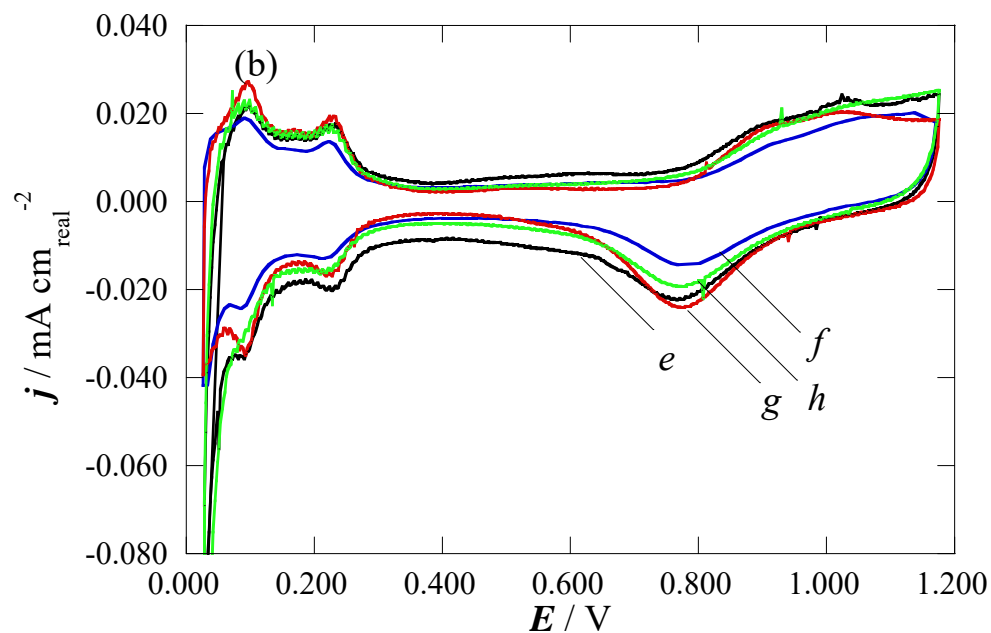
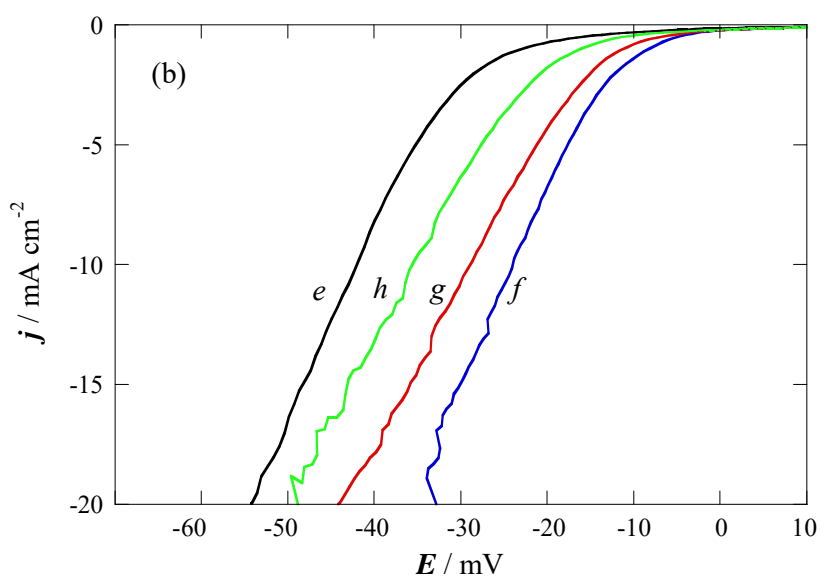
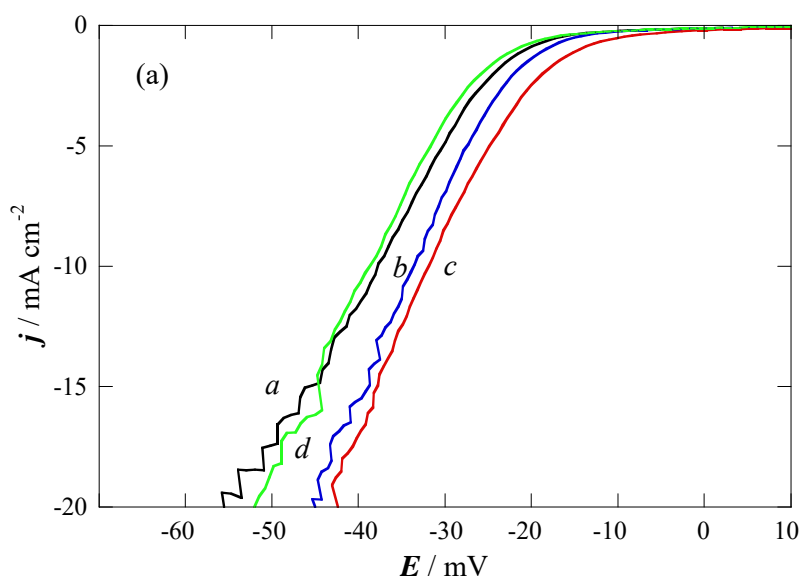


Fig. 7 – Cyclic voltammograms in deaerated $0.50 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4$ at 20 mV s^{-1} for 20 wt % Pt on (a) TiO_2 -based and (b) TNTs-based supports. Figure (c) corresponds to commercial Pt/C compared to Pt supported on TiO_2 and TNTs. The different j - E curves correspond to (a) Pt/ TiO_2 , (b) Pt/3Nb- TiO_2 , (c) Pt/6Nb- TiO_2 , (d) Pt/10Nb- TiO_2 , (e) Pt/TNT, (f) Pt/3Nb-TNT, (g) Pt/6Nb-TNT, (h) Pt/10Nb-TNT, (i) commercial Pt/C, (j) Pt/6Nb- TiO_2 and (k) Pt/6Nb-TNT. IR-drop corrected. The current densities have been referred to the corresponding ECSAs.

Fig. 8a and b depicts the linear sweep voltammograms corresponding to the HER in deaerated $0.50 \text{ mol dm}^{-3} \text{ H}_2\text{SO}_4$ at 1 mV s^{-1} on Pt deposited on the TiO_2 -based and the TNTs-based supports, respectively. All the curves shown in Fig. 8a and b start with an exponential current density increase with potential. However, for current densities above 10 mA cm^{-2} , the hydrogen bubbles evolved from the working electrode significantly affected the shape of j - E curves. Note that these curves move in a potential range of about 10 and 20 mV for the TiO_2 (Fig. 8a) and TNTs supports (Fig. 8b), respectively. As long as the experimental error was better than 5 mV, the different j - E plots denoted different catalyst activity, despite the Pt nanoparticles have about the same size and ECSA, on all the supports studied (see Table 2). This different performance could then be explained by a different Pt-support interaction, which depended on the support. Nb doping of TiO_2 and TNTs generally led to better electrocatalyst activity, what can be explained by the local increase of the electron density on Pt due to the SMSI discussed above, favored by the Nb doping, in particular for the TNTs. It is apparent from the j - E plots of Fig. 8a and b that the Pt catalysts supported on TiO_2 and TNTs doped with 3 and 6 at % Nb showed the highest catalytic activity, because the current densities at a given potential were greater than for the other supports. Some reduction in the catalyst activity is observed when Nb doping increases to 10 at %. This is probably related to the pore diameter decrease when increasing the Nb doping, despite that the specific surface area increased, feature that can limit the accessibility to the nanoparticles.

From a quantitative point of view, it is useful to provide some characteristic parameters used to evaluate the HER performance of the different catalysts, such as the potential required to achieve a current density relevant for the electrolyzer design [54,78,79]. Thus, the potential required to achieve a $j = -0.010 \text{ A cm}^{-2}$ (E_{10}) were measured for each catalyst studied in this paper and the corresponding results have been compared in Table 3. The

values reported in this table for the most positive E_{10} indicate that the best catalytic activity corresponds to Pt/3Nb-TNT, followed by Pt/6Nb-TNT, Pt/6Nb-TiO₂ and Pt/3Nb-TiO₂, with E_{10} values of -0.024, 0.029, -0.032 and -0.034 V, respectively. These values are more positive than those corresponding to pristine TiO₂ and TNTs, which are of -0.038 and -0.042, also respectively.



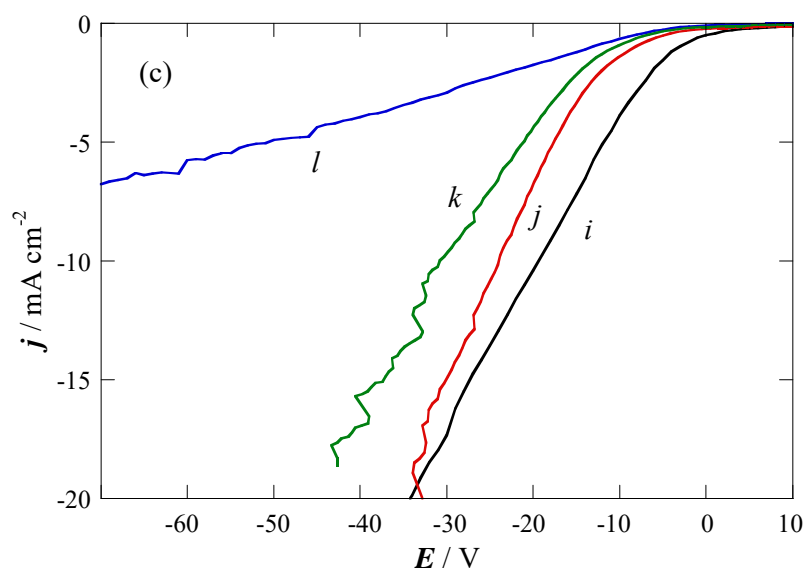


Fig. 8 – j - E curves corresponding to the HER in 0.50 mol dm⁻³ H₂SO₄ at 1 mV s⁻¹ on 20 wt % Pt on (a) TiO₂-based, (b) TNTs-based supports and (c) comparison with commercial Pt/C. The different j - E curves correspond to (a) Pt/TiO₂, (b) Pt/3Nb-TiO₂, (c) Pt/6Nb-TiO₂, (d) Pt/10Nb-TiO₂, (e) Pt/TNTs, (f) Pt/3Nb-TNTs, (g) Pt/6Nb-TNTs, (h) Pt/10Nb-TNTs, (i) commercial Pt/C, (j) Pt/3Nb-TNT, (k) Pt/3Nb-TNT normalized to the ECSA and (l) commercial Pt/C normalized to the ECSA. IR-drop corrected. The current density has been referred to the electrode section except in curves (k) and (l).

It is interesting to compare the performance of the catalysts reported in this paper with published data relative to Pt deposited on other supports and to commercial carbon-supported Pt. This comparison is not straightforward because of the variety of Pt loadings and experimental conditions used to assess the HER catalyst activity. However, some comparisons can be established in terms of the E_{10} defined above (see Table 3), obtained from the LSV curves corrected by the ohmic drop, and Tafel slopes. Thus, Bhowmik et al [54] reported the HER on Pd-CN_x and commercial 10 wt % Pt/C in 0.50 M H₂SO₄. The E_{10} of the latter was about -0.058 V and the Tafel slope was 0.033 V dec⁻¹. Yang et al

[80] developed PtCo alloy nanoparticles encapsulated in carbon nanofibers for electrochemical hydrogen generation. From the reported j - E curves for HER in 0.50 M H₂SO₄, the E_{10} values obtained for PtCo/CNFs (5 wt % Pt) and Pt/CNF (8.5 wt % Pt) were -0.063 and -0.104 V, respectively. In the same work it was reported an E_{10} of about -0.057 V for commercial 20 wt. % Pt/C (Johnson-Matthey). Wang et al [40] developed monodisperse 20 wt. % Pt on N-doped black TiO₂ as high performance bifunctional catalyst. The E_{10} for the HER was about -0.035 V in 0.10 M H₂SO₄, reporting a Tafel slope of 0.033 V dec⁻¹. It was also shown an E_{10} value of 0.040 V for Pt/TiO₂ with a Tafel slope of 52 mV dec⁻¹, which is remarkably coincident with our results for Pt/TiO₂ and Pt/TNT, which are 0.040 ± 0.002 V. Zhang et al [81] synthesized a Pt/WS₂ (10 wt % Pt) catalyst for enhanced hydrogen evolution reaction. According to the experimental data, in N₂-saturated 0.50 M H₂SO₄, E_{10} was of -0.080 V with a Tafel slope of 0.055 V dec⁻¹. In the same paper, the same value of E_{10} of -0.080 V was given for Pt deposited on activated charcoal. It is also interesting to list the E_{10} value of -0.075 V for the Pt foil reported by Liu et al [43].

Due to the variety of the experimental conditions and the dispersion of values, the measurement of E_{10} was also performed for commercial Pt/C in the same conditions as those for the titania-supported catalysts. As indicated in Table 3 and shown in Fig. 8c, curve *i*, E_{10} was -0.020 V, which is more positive than that of Pt/3Nb-TNT (curve *j* in Fig. 8c). This value is closer to the value of -0.027 and -0.022 V reported recently for Pt/C and Pt-NCS [5]. However, the Pt/C catalyst used in this paper had higher ECSA than those of the titania-supported catalysts, 43 m² g_{Pt}⁻¹ in front of 11-14 m² g_{Pt}⁻¹, respectively. Therefore, the current densities referred to the ECSA should be more relevant to compare the catalysts activities. The corresponding figures were also plotted in Fig. 8c, curves *k* and *l*, for Pt/3Nb-TNT and Pt/C, respectively. It is apparent that when the current densities

are normalized to the ECSA, Pt/3Nb-TNT appears to be more active than Pt/C. These data strongly indicate the importance of the Pt support and confirm the good activity towards HER of Pt deposited on the TiO₂ and TNTs supports developed in this work. This good activity combined with its stability against corrosion by oxygen crossover, as shown by the oxygen evolution reaction studies on TiO₂ supports [29], makes Pt/Nb-TNT very promising as catalysts for the HER in PEMWEs. Although out of the scope of the present paper, stability tests are in perspective in real PEMWEs.

Table 3 – Electrode potential corresponding to a current density of 10 mA cm⁻² in the steady linear sweep voltammograms (corrected by the *IR*-drop) of the HER in acidic media, 0.50 M H₂SO₄ unless otherwise indicated, on Pt deposited on different supports.

Electrocatalyst	Pt content / wt %	Pt loading / $\mu\text{g cm}^{-2}$	E_{10} / V	Reference
Pt/TiO ₂	20	14.0	-0.038	This work
Pt/3Nb-TiO ₂	20	14.0	-0.034	Id.
Pt/6Nb-TiO ₂	20	14.0	-0.032	Id.
Pt/10Nb-TiO ₂	20	14.0	-0.039	Id.
Pt/TNT	20	14.0	-0.042	Id.
Pt/3Nb-TNT	20	14.0	-0.024	Id.
Pt/6Nb-TNT	20	14.0	-0.029	Id.
Pt/10Nb-TNT	20	14.0	-0.036	Id.
Pt/C (Premetek)	20	14.0	-0.020	Id.
Pt/C (Sigma-Aldrich)	10	42.0	-0.058	[54]
PtCo/CNF	5	15.7	-0.063	[80]
Pt/CNF	8.5	18.0	-0.104	[80]
Pt/C (Johnson-Matthey)	20	42.5	-0.057	[80]
Pt/TiO ₂ ^a	20	50.0	-0.040	[40]
Pt/N _x :TiO _{2-x} ^a	20	50.0	-0.035	[40]
Pt/WS ₂	10	^b	-0.080	[81]
Pt/activated charcoal	10	^b	-0.080	[81]

Pt foil	100	-	-0.075	[43]
Pt/C	20	$-^b$	-0.027	[5]
Pt-NCS ^c	$-^b$	$-^b$	-0.022	[5]
Pt-CS ^d	$-^b$	$-^b$	-0.041	[5]

^a 0.10 M H₂SO₄.

^b not reported.

^c Pt nanoparticles embedded in N-enriched carbon matrix.

^d Pt nanoparticles embedded in carbon matrix

The cathodic Tafel slope (b_c) has also been used as an indicative result of the catalytic activity, because in general, smaller Tafel slopes are obtained for catalysts with high charge transfer ability [40,54,82]. The generally established HER mechanism consists of an initial discharge step (1) followed by either an electrochemical desorption step (2) or a chemical recombination step (3). These steps are known as the Volmer, Heyrovsky and Tafel reactions, respectively, which can be written as follows:



Depending on the rate-determining-step (rds), the values of b_c for Volmer, Heyrovsky and Tafel reactions are of 0.118, 0.040 and 0.029 V dec⁻¹, respectively [79].

Fig. 9a and b shows the E vs. $\log j$ plots for Pt deposited to 20 wt % on the Nb-doped TiO₂ and TNTs, respectively. As shown in this figure, values close to 0.030 V dec⁻¹ were obtained for all the catalysts.

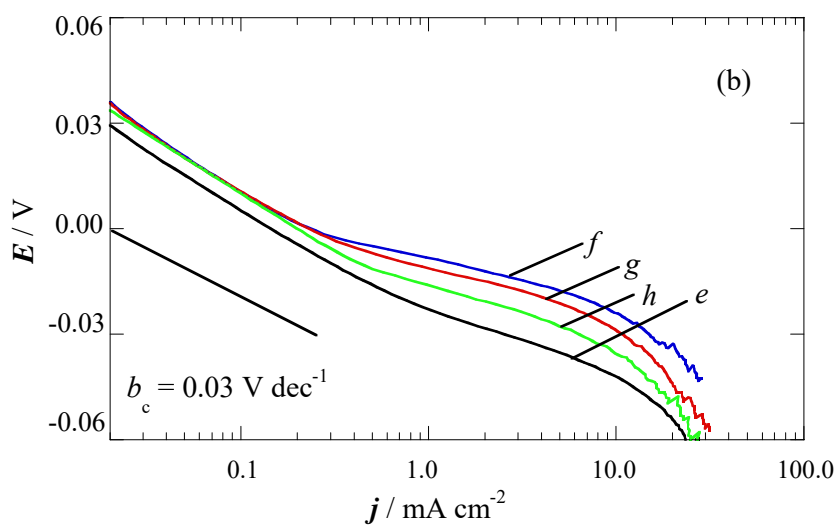
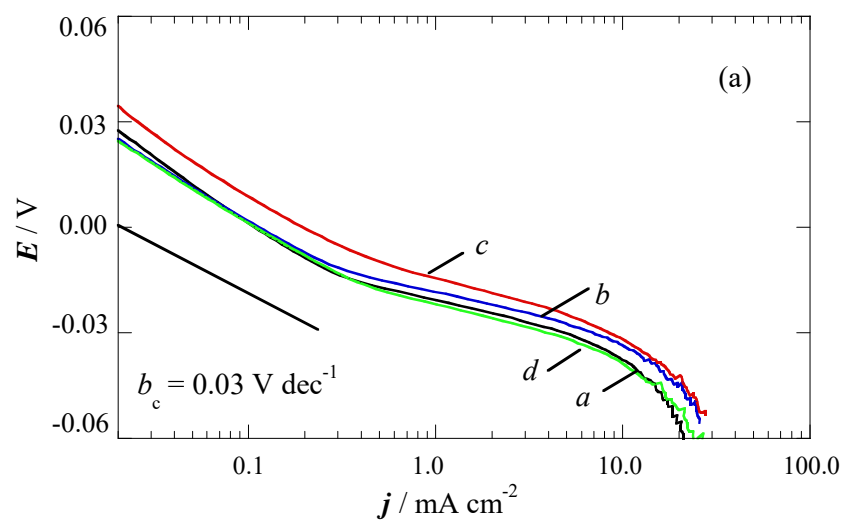


Fig. 9 –Tafel plots corresponding to the linear sweep voltammograms depicted in (a) Fig. 8a and (b) Fig. 8b. A Tafel slope of 0.03 V dec^{-1} has been drawn for comparison.

These values of the Tafel slopes indicate that the HER follows a Volmer-Tafel mechanism, the rds being the Tafel reaction, in agreement with previous results reported

in the literature for the HER on polycrystalline Pt-based catalysts [83]. It can be then suggested that the SMSI leading to a negative charge accumulation on Pt also facilitates the hydrogen desorption and therefore, it allows increasing the rate of the Tafel reaction.

4. Conclusions

Nb-doped TiO₂ and Nb-doped TNTs were synthesized and characterized to be used as supports of Pt nanoparticles for the HER electrocatalysis in water electrolysis. The specific surface areas of the Nb-doped TiO₂ support were in the range 87-100 m²g⁻¹, whereas greater values of 260-303 m²g⁻¹ were achieved for Nb-doped TNTs. The presence of Nb increased the specific surface area of TiO₂ and TNTs. The lattice parameters, determined from XRD, showed the lattice expansion of titania with increasing the Nb doping. Also shown by the XRD results, the Pt nanoparticles deposited up to 20 wt % on the TiO₂ and TNTs supports had crystallite sizes of about 4-5 nm. The corresponding XPS analyses indicated a local increase of the electron density on Pt when supported on titania compared to Pt/C, which was attributed to the stronger interaction of Pt with the titania supports.

The electrochemical characterization towards HER in deaerated 0.50 mol dm⁻³ H₂SO₄ aqueous solution showed the good performance of the Pt electrocatalysts prepared with Nb-doped TiO₂ and TNTs supports, with higher catalytic activity per unit of electroactive surface area than that of commercial Pt/C. These results make the Pt/Nb-TNT catalysts, in particular that containing 3 at % Nb, very promising to be applied for the hydrogen evolution reaction in proton exchange membrane water electrolyzers.

Acknowledgements

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