

# **EFFECTS OF SYNTHESIS METHODS AND PARAMETERS ON SODIUM ZIRCONATE FOR HIGH-TEMPERATURE CO<sub>2</sub> SORPTION**

**OOI KHIM MAY**

**UNIVERSITI SAINS MALAYSIA**

**2015**

**EFFECTS OF SYNTHESIS METHODS AND  
PARAMETERS ON SODIUM ZIRCONATE FOR  
HIGH-TEMPERATURE CO<sub>2</sub> SORPTION**

**by**

**OOI KHIM MAY**

**Thesis submitted in fulfillment of the requirements  
for the degree of  
Master of Science**

**October 2015**

## ACKNOWLEDGEMENTS

First of all, my utmost appreciation goes to my main supervisor from Universiti Sains Malaysia (USM), Prof. Dr. Abdul Rahman bin Mohamed, and co-supervisor from Monash University Malaysia, Dr. Chai Siang Piao, for accepting me as their postgraduate student. Without their supervision and guidance, I would have been lost in direction in undertaking my research activities.

Furthermore, I would like to acknowledge the financial supports given by USM through the Research University-Postgraduate Research Grant Scheme (USM-RU PRGS) (1001/PJKIMIA/8035017) and Research University Team (RUT) (1001/PJKIMIA/854001), and the Ministry of Higher Education (MOHE) Malaysia through the Long-term Research Grant Scheme (LRGS) (203/PKT/6723001) and MyMaster scholarship. These grants and scholarship have been a great help throughout my whole postgraduate studies in reducing the financial burden for self-support and to perform my research activities.

I am very grateful to the administrative staff and laboratory technicians from School of Chemical Engineering, School of Materials and Mineral Resources Engineering, and School of Physics in USM, and School of Engineering in Monash University Malaysia for their technical support and assistance. My utmost gratitude also goes to Mr. Karunakaran and En. Mohamed Mustaqim from the X-ray Crystallography Lab in School of Physics in USM for the discussions and guidance in analysing the XRD results.

Last but not least, my sincere gratitude goes to all of my family members and friends, of whom too many are to be named here. Their endless moral support, company, motivation, guidance and assistance in research and non-research related issues have led me to persevere to the very end of my research studies.

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## LIST OF SYMBOLS

|              |                                  |
|--------------|----------------------------------|
| $\Delta$     | heat-treated reaction            |
| $\Delta H_f$ | enthalpy of formation            |
| $\theta$     | theta                            |
| $(P/P_0)$    | relative partial pressure        |
| $E_a$        | activation energy                |
| $P_{CO_2}$   | CO <sub>2</sub> partial pressure |
| $T$          | temperature                      |

## LIST OF ABBREVIATIONS

|          |   |
|----------|---|
| AC       | activated carbon                                  |
| APTS     | 3-aminopropyl-triethoxysilane                     |
| aq       | aqueous   |
| BET      | Brunauer-Emmett-Teller                            |
| CA       | citric acid/citrate                               |
| ca.      | approximately/calculated                          |
| CNTs     | carbon nanotubes                                  |
| CTAB     | cetyl trimethylammonium bromide                   |
| DI water | deionized water                                   |
| DSC      | differential scanning calorimetry                 |
| EG       | ethylene glycol                                   |
| FTIR     | Fourier transform infrared                        |
| GHG      | greenhouse gas                                    |
| HTC      | hydrotalcite                                      |
| ICDD     | International Centre for Diffraction Data         |
| IEA      | International Energy Agency                       |
| IPCC     | International Panel on Climate Change             |
| IUPAC    | International Union of Pure and Applied Chemistry |
| LDH      | layered double hydroxide                          |
| MNRE     | Ministry of Natural Resources and Environment     |
| MOFs     | metal organic frameworks                          |
| MS       | mass spectrometry                                 |
| NaCA     | trisodium citrate                                 |
| PSA      | pressure swing adsorption                         |
| RDS      | rate determining step                             |
| SEM      | scanning electron microscope/microscopy           |
| SESMR    | sorption enhanced steam methane reaction          |
| TGA      | thermogravimetric analyser/analysis               |

TSA      temperature/thermal swing adsorption  
XRD      X-ray diffraction/diffractometer

# KESAN-KESAN PENGUBAHAN KAEDAH DAN PARAMETER SINTESIS TERHADAP NATRIUM ZIRKONAT UNTUK PENJERAPAN CO<sub>2</sub> BERSUHU TINGGI

## ABSTRAK

Pemancaran karbon dioksida (CO<sub>2</sub>) ialah antara punca-punca pemanasan sejagat. Penangkapan CO<sub>2</sub> secara penjerapan CO<sub>2</sub> telah menjadi salah satu kaedah untuk mengurangkan pemancaran CO<sub>2</sub>. Tambahan pula, penjerap yang bercekapan tinggi diperlukan untuk penangkapan CO<sub>2</sub> bersuhu tinggi daripada proses-proses industri hibrid. Natrium zirconat (Na<sub>2</sub>ZrO<sub>3</sub>) ialah salah satu bahan penjerap pepejal yang berpotensi dan mempunyai prestasi penjerapan berkisar CO<sub>2</sub> yang tinggi dan stabil, tetapi kapasiti jerapan CO<sub>2</sub> yang lebih dekat dengan kapasiti unggul masih dikehendaki. Tambahan pula, kesan-kesan metodologi yang berbeza terhadap prestasi penangkapan CO<sub>2</sub> dengan penjerap ini belum dilaporkan dalam kajian-kajian terdahulu. Tujuan utama penyelidikan ini ialah menambah baik sintesis dan oleh itu kapasiti jerapan CO<sub>2</sub> untuk penjerapan CO<sub>2</sub> bersuhu tinggi dengan bahan penjerap Na<sub>2</sub>ZrO<sub>3</sub>. Kesan-kesan keadaan pengkarbonatan dan pengkalsinan, prekursor natrium (Na) yang berbeza dan penambahan asid sitrik (CA) dan etilena glikol (EG) terhadap Na<sub>2</sub>ZrO<sub>3</sub> yang disintesis dan oleh itu prestasi penjerapan CO<sub>2</sub> bersuhu tinggi telah disiasat. Ujian pencirian dan prestasi penjerapan CO<sub>2</sub> terhadap sampel-sampel ini dilakukan melalui analisis termogravimetri, pembelauan sinar-X, penjerapan N<sub>2</sub> dan SEM. Semua parameter-parameter tersebut memberi kesan-kesan yang ketara terhadap prestasi penjerapan CO<sub>2</sub> untuk bahan penjerap Na<sub>2</sub>ZrO<sub>3</sub> yang disediakan. Kegunaan prekursor Na yang berbeza dan suhu penjerapan CO<sub>2</sub> mempengaruhi kapasiti penjerapan CO<sub>2</sub> sampel-sampel itu. Keadaan kalsinasi yang berbeza juga memperanguhi ketulenan bahan penjerap Na<sub>2</sub>ZrO<sub>3</sub>. Penambahan CA dan EG menghasilkan bahan penjerap Na<sub>2</sub>ZrO<sub>3</sub> yang lebih tulen, mempunyai morfologi yang lebih berliang dan oleh itu kestabilan penajaan semula penjerap ini yang lebih baik daripada sampel yang disediakan tanpa penambahan CA dan EG. 4.902 mmol/g Na<sub>2</sub>ZrO<sub>3</sub>, iaitu kapasiti penjerapan CO<sub>2</sub> yang terbaik, telah dicapai



pada suhu pengkarbonatan 550 °C untuk sampel yang disintesis dengan natrium sitrat sebagai prekursor Na serta menggunakan CA dan EG dengan nisbah molar 2:1, dan dikalsin pada 900 °C selama 4 h. Oleh itu, penjerap ini adalah sesuai untuk penangkapan CO<sub>2</sub> bersuhu tinggi. Ujian keberangkapan di bawah keadaan perindustrian untuk bahan penjerap Na<sub>2</sub>ZrO<sub>3</sub> ini yang telah bertambah baik adalah dicadangkan.

# EFFECTS OF SYNTHESIS METHODS AND PARAMETERS ON SODIUM ZIRCONATE FOR HIGH-TEMPERATURE CO<sub>2</sub> SORPTION

## ABSTRACT

Carbon dioxide (CO<sub>2</sub>) emission is among the causes of global warming. CO<sub>2</sub> capture by CO<sub>2</sub> adsorption has been one of the methods to reduce CO<sub>2</sub> emission. Moreover, an adsorbent with high efficiency is needed for high-temperature CO<sub>2</sub> capture from industrial hybrid processes. Sodium zirconate (Na<sub>2</sub>ZrO<sub>3</sub>) is one of the potential solid sorbents with high and stable cyclic CO<sub>2</sub> sorption performance, but CO<sub>2</sub> adsorption capacity closer to its ideal capacity is still desired. Furthermore, the effects of different methodologies on its CO<sub>2</sub> capture performance were not reported previously. The main aim of this research work is to improve the synthesis and thus CO<sub>2</sub> capture capacity of Na<sub>2</sub>ZrO<sub>3</sub> for high-temperature CO<sub>2</sub> sorption. Effects of carbonation and calcination conditions, different sodium (Na) precursors, and addition of citric acid (CA) and ethylene glycol (EG) on high-temperature CO<sub>2</sub> sorption performance of synthesised Na<sub>2</sub>ZrO<sub>3</sub> were investigated. Characterisation and CO<sub>2</sub> sorption performance of samples were tested using thermogravimetric analysis, X-ray diffraction, N<sub>2</sub> adsorption and SEM. All the above-mentioned parameters significantly affect the CO<sub>2</sub> adsorption performances of the prepared Na<sub>2</sub>ZrO<sub>3</sub> sorbents. The use of different Na precursor and CO<sub>2</sub> adsorption temperature influenced the CO<sub>2</sub> adsorption capacity of the samples. Different calcination conditions also affected the purity of Na<sub>2</sub>ZrO<sub>3</sub>. Addition of CA and EG resulted in producing purer Na<sub>2</sub>ZrO<sub>3</sub> with more porous morphology and hence better regeneration stability than the sample prepared without the addition of CA and EG. The best CO<sub>2</sub> adsorption capacity of 4.902 mmol CO<sub>2</sub>/g Na<sub>2</sub>ZrO<sub>3</sub> was achieved at carbonation temperature of 550 °C, for the sample synthesised with sodium citrate as the Na precursor and CA:EG molar ratio of 2:1, and calcined at 900 °C for 4 h. Hence, this sorbent is suitable for high-temperature CO<sub>2</sub> capture. It is recommended to test the functionality of this improved Na<sub>2</sub>ZrO<sub>3</sub> sorbent under industrial conditions.

## CHAPTER 1

### INTRODUCTION

#### 1.1 Carbon dioxide and its emission

Carbon dioxide (CO<sub>2</sub>) is one of the gases present in the atmosphere. It is an important source for photosynthesis and production of useful chemicals, for example cyclic carbonates and organic carbonates (Ma, *et. al.*, 2009; MacDowell *et. al.*, 2010). This gas is produced from natural activities such as respiration of human beings and animals, and anthropogenic sources such as combustion of petroleum and manufacturing industries with CO<sub>2</sub> as one of the secondary products.

CO<sub>2</sub> takes up approximately 0.03% of the total air composition, but this composition has been varying since the Industrial Revolution in mid-18<sup>th</sup> century due to increasing industrial and human-related activities and thus increasing energy generation from fossil fuel combustion (Wilcox, 2012; Hartmann *et. al.*, 2013). Continuous large emissions of CO<sub>2</sub>, which is also a greenhouse gas (GHG), have led to global warming. The International Energy Agency (IEA) reported that global CO<sub>2</sub> emissions reached 31734 million tonnes in the year 2012, which was the last reported year and the highest among all the reported years by IEA (IEA, 2014). The seriousness of the negative impacts of global warming on climate change have led governments, environmental bodies and researchers to put in extra efforts and investigate ways of reducing CO<sub>2</sub> emissions and consequently mitigating GHG effects, namely, melting of glaciers and natural disasters such as drought and floods.

## **1.2 Current technologies for CO<sub>2</sub> capture**

Various solutions have been considered to combat the problems of increasing CO<sub>2</sub> emissions. One of these solutions is CO<sub>2</sub> capture which works on the simple concept of CO<sub>2</sub> sorption from flue gas and other production sources before its emission to the atmosphere. The captured CO<sub>2</sub> will then be desorbed from the sorbents before the gas is either used as a feedstock for conversion to useful raw materials like urea and carbon-based fuels such as methanol and methane, or sequestered in depleted oil and gas reservoirs (Ma *et. al.*, 2009; MacDowell *et. al.*, 2010).

Several methods for CO<sub>2</sub> capture have been studied to reduce CO<sub>2</sub> concentration in waste gas emissions and thus combat the issues of global warming. These methods include CO<sub>2</sub> sorption by amine-based solvent stripping, membrane separation, cryogenic distillation and oxyfuel combustion. These methods have been applied in industrial applications, generally, for feasible reasons such as low operation costs and the removal of CO<sub>2</sub> gas with high purity. However, the presence of impurities such as moisture, NO<sub>x</sub> and SO<sub>x</sub> gases in the gas stream and fluctuating process conditions lead to corrosion of equipment and deterioration of the medium used for the separation of CO<sub>2</sub> from the gas stream. Besides that, the CO<sub>2</sub> selectivity of these separation processes is still considerably low. The temperature range used for CO<sub>2</sub> absorption and membrane separation is limited to below 500 °C to prevent deterioration of the solvent and membrane respectively (Aaron and Tsouris, 2005; Yang *et. al.*, 2008; Nair *et. at.*, 2009; MacDowell *et. al.*, 2010; Pires *et. al.*, 2011; Wilcox, 2012).

## **1.3 CO<sub>2</sub> capture by solid-based adsorbents**

In addition to the methods as mentioned above, CO<sub>2</sub> capture using solid adsorbents has also been used in several industrial applications such as post-combustion flue gas cleaning and pre-combustion hydrogen gas (H<sub>2</sub>) production by sorption enhanced steam methane reaction

(SESMR). Some of the reasons are the lower requirements of energy usage, operating costs, and equipment, and higher and wider operating temperature range from ambient temperature to about 700 °C than the above-mentioned technologies. Furthermore, generation of liquid wastes can be avoided and spent adsorbents can be discarded without environmental concerns (Harrison, 2005; Ochoa-Fernández *et al.*, 2007; Hao *et al.*, 2011; Pires *et al.*, 2011).

Practicability and sustainability of CO<sub>2</sub> capture using solid sorbents is currently among the research fields of interest to improve the efficiencies of CO<sub>2</sub> sorbents. Carbon-based materials such as carbon nanotubes and activated carbons, zeolites and amine-functionalised silica materials are a few examples of solid sorbents. Ideally, a good CO<sub>2</sub> solid sorbent should be a corrosion-resistive material with high CO<sub>2</sub> selectivity, and adsorption and desorption capacities with fast kinetics. It should also exhibit high regeneration stability and durability at industrial operating conditions with low operating pressures and CO<sub>2</sub> partial pressures (Yong *et al.*, 2002; Deng 2006; Choi *et al.*, 2009; Sayari *et al.*, 2011). However, the above-mentioned materials are generally unsuitable for applications in high-temperature or impure gas streams, have low CO<sub>2</sub> adsorption capacities, or could not be regenerated repetitively (Choi *et al.*, 2009; Hao *et al.*, 2011; Sayari *et al.*, 2011; Q. Wang *et al.*, 2011).

#### **1.4 Sodium zirconate as a potential CO<sub>2</sub> sorbent**

Researchers have considered sodium zirconate (Na<sub>2</sub>ZrO<sub>3</sub>) as one of the most promising materials to effectively remove CO<sub>2</sub> from flue gas. This is due to its reusability and favourable thermodynamics of the whole CO<sub>2</sub> sorption process. Na<sub>2</sub>ZrO<sub>3</sub> is one of the known adsorbents that can capture CO<sub>2</sub> gas at high temperatures of above 400 °C, which is applicable for post-combustion reactions and sorption-enhanced H<sub>2</sub> production. It has better regeneration stability than calcium oxide (CaO), higher CO<sub>2</sub> uptake than lithium zirconate (Li<sub>2</sub>ZrO<sub>3</sub>) and works well in wet gas streams (López-Ortiz *et al.*, 2004; Santillán-Reyes and

Pfeiffer, 2011; Wang Q *et. al.*, 2011). This alkaline mixed metal-oxide ceramic compound is known to react with CO<sub>2</sub> gas in a reversible exothermic reaction as described in equation (1.1) (López-Ortiz *et. al.*, 2004; Ochoa-Fernández *et. al.*, 2009):



Research studies on this material for CO<sub>2</sub> capture are rarely reported compared to Li<sub>2</sub>ZrO<sub>3</sub>, which is the other zirconate compound of interest. López-Ortiz *et. al.* (2004) compared the capability of Na<sub>2</sub>ZrO<sub>3</sub> with other sodium and lithium-containing oxides, including Li<sub>4</sub>SiO<sub>4</sub> and Li<sub>2</sub>ZrO<sub>3</sub>, for CO<sub>2</sub> sorption and found that Na<sub>2</sub>ZrO<sub>3</sub> has better overall CO<sub>2</sub> capture performance than Li<sub>4</sub>SiO<sub>4</sub> and Li<sub>2</sub>ZrO<sub>3</sub>. Besides that, Na<sub>2</sub>ZrO<sub>3</sub> prepared with excess sodium precursor can adsorb and desorb a very high amount of CO<sub>2</sub> close to the stoichiometric capacity of 5.400 mmol/g. Its CO<sub>2</sub> sorption rate of 2.348 mmol g<sup>-1</sup> min<sup>-1</sup> is also the fastest among all the potential CO<sub>2</sub> adsorbents (López-Ortiz *et. al.*, 2004).

## 1.5 Problem statements

Na<sub>2</sub>ZrO<sub>3</sub> solid sorbents were successfully developed for high-temperature CO<sub>2</sub> capture applications. The highest reported CO<sub>2</sub> adsorption capacity of Na<sub>2</sub>ZrO<sub>3</sub> thus far was 4.901 mmol/g (Radfarnia and Iliuta, 2012). However, its CO<sub>2</sub> adsorption capacity decreased with increasing number of cycles for 4 cycles. Hence, it is still desirable to produce a Na<sub>2</sub>ZrO<sub>3</sub> solid sorbent with CO<sub>2</sub> adsorption capacity that is closer to the theoretical amount of 5.400 mmol/g and is consistent for numerous number of cycles for an even higher removal of CO<sub>2</sub> gas. This could be done by comparison of preparation methods.

Synthesis of Na<sub>2</sub>ZrO<sub>3</sub> sorbent has been done, most commonly, by solid-state reaction between the Na<sub>2</sub>CO<sub>3</sub> and ZrO<sub>2</sub> precursors. Na<sub>2</sub>ZrO<sub>3</sub> has also been developed successfully by simple liquid-state reaction (Zhao *et. al.*, 2007; 2013) and surfactant-template/sonication method (Radfarnia and Iliuta, 2012). Na<sub>2</sub>ZrO<sub>3</sub> has also been produced by sol-gel synthesis

for other applications such as coating of metallic biomedical implants (Subrasi *et. al.*, 2002; Devi and Rajendran, 2012). Sol-gel method is known to produce materials with high purity and improved particle characteristics. The Pechini method is the preferred sol-gel method due to its simple and inexpensive methodology (Petrykin and Kakihana, 2005). Currently, the Pechini sol-gel synthesis of  $\text{Na}_2\text{ZrO}_3$  sorbent for the application of  $\text{CO}_2$  capture is yet to be reported.

In this research, development of  $\text{Na}_2\text{ZrO}_3$  sorbent with improved  $\text{CO}_2$  sorption characteristics was attempted. This was done by varying various synthesis and  $\text{CO}_2$  sorption parameters, and comparing synthesis methods to investigate their effects on the  $\text{CO}_2$  sorption performance of the prepared  $\text{Na}_2\text{ZrO}_3$  sorbents. It is anticipated that this solid sorbent with improved  $\text{CO}_2$  adsorption properties could be produced.

## **1.6 Research objectives**

The aims of this research are:

- 1) To improve the synthesis parameters for the development of  $\text{Na}_2\text{ZrO}_3$  as a  $\text{CO}_2$  solid sorbent with improved characteristics,
- 2) To investigate the  $\text{CO}_2$  sorption performance of the above-synthesised  $\text{Na}_2\text{ZrO}_3$  sorbent, and
- 3) To study the usability and stability of the above-prepared  $\text{Na}_2\text{ZrO}_3$  for multicyclic high-temperature  $\text{CO}_2$  capture.

## **1.7 Research scope**

This research work focuses on the preparation of  $\text{Na}_2\text{ZrO}_3$  as a  $\text{CO}_2$  solid sorbent by liquid-state reaction and Pechini sol-gel synthesis methods for the purpose of improving its  $\text{CO}_2$  sorption performance. At the synthesis stage, calcination methods, sodium precursors and

ratios of additional gelling agents were varied. The synthesised  $\text{Na}_2\text{ZrO}_3$  was then tested for its  $\text{CO}_2$  capture performance using the thermogravimetric analyser (TGA) in pure  $\text{CO}_2$  gas for every variation of parameters during the preparation and carbonation stages. TGA was used for one-factor-at-a-time screening of the synthesised  $\text{Na}_2\text{ZrO}_3$ . Finally, the sample with the best  $\text{CO}_2$  sorption performance was analysed for its structural characteristics and regeneration stability.

## 1.8 Thesis outline

The organisation of this thesis starts off with **Chapter 1** to introduce the readers about  $\text{CO}_2$  as a greenhouse gas, current statistics of its emission, and issues faced by governments and scientists to combat greenhouse gas effects, particularly  $\text{CO}_2$  gas reduction. The concept, current technologies and difficulties of  $\text{CO}_2$  adsorption are also briefly discussed in this chapter. With this, the research objectives and scope are outlined here.

**Chapter 2** gives readers an insight on the theories and concepts involved in this research work. Various methods and results obtained by different scientists to prepare  $\text{Na}_2\text{ZrO}_3$  as a  $\text{CO}_2$  solid sorbent are also compiled in this chapter.

Details of the experimental and analytical methods done in this work to synthesise and characterise the prepared  $\text{Na}_2\text{ZrO}_3$  respectively for  $\text{CO}_2$  sorption are described in **Chapter 3**, whereas **Chapter 4** discusses the results obtained in this research work and the explanations behind these findings.

Lastly, **Chapter 5** concludes the experimental results and discussions of this research work in this thesis, together with future recommendations of this research study.