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Recovery of humic acids from anaerobic sewage sludge: Extraction, characterization and encapsulation in alginate beads

Original

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(Article begins on next page)

1 Title:

- 2 Recovery of humic acids from anaerobic sewage sludge: extraction, characterization and
- 3 encapsulation in alginate beads

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16 Highlights:

- Humic acids extraction from sewage sludge anaerobically digested
- Humic acids extracted without heavy metals
- Study of humic acids molecular weight in the extract
- Encapsulation of humic acids within alginate beads for controlled releasing in soil
- Humic acids beads allows roots biomass enhancement in greenhouse experiment

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23 Graphical abstract: (in colors)

Anaerobic sewage sludge HA extract Test of fertilizing effects encapsulation in greenhouse experiment in alginate beads Humic acids (HA) HA extract ight (MW) Molecular extraction FESEM-EDX analysis of HA quantification and molecular size distribution HA extract and beads

25

26 Abstract:

Wastewater production is rising all over the world and one of the most difficult problems is the disposal of sewage sludge (SS). It is known that SS contains certain quantities of added-value compounds, such as humic acids (HA) which in turn have beneficial effects on soil quality and plant

growth. On the other hand, SS can retain many pollutants, such as heavy metals. The present work 30 31 aimed to implement an HA alkaline extraction protocol from anaerobic sewage sludge (ASS). 32 Subsequently, the HA were quantified in ASS, in HA extract and in commercial HA, used as a benchmark, which gave results of 12.53%, 26.87% and 77.87% (on dry matter basis), respectively. 33 FESEM and EDX analyses on lyophilized HA extract confirmed that no heavy metals had passed 34 into the extract. Afterwards, in order to allow controlled release of the HA in soils, alginate beads 35 containing the HA extract were created. Finally, a pot experiment in a greenhouse was performed 36 37 using Chilean lettuce plants (Lactuca sativa L.) treated with alginate-HA extract beads. At the end of the greenhouse experiments, the hypogean dry biomass of the treated plants was significantly higher 38 than for non-treated plants. The relevance of this study relies not only on the exploitation of green 39 40 chemistry principles, by converting a waste stream into a high-value product, but also on the 41 application of an approach following a circular economy model.

- 42 Keywords: humic acids extraction, circular economy, greenhouse experiment
- 43 **Declaration of interest:** none.

44 Glossary of abbreviations and acronyms

Abbreviation	Definition
ANOVA	Analysis Of Variance
ASS	Anaerobic Sewage Sludge
ATR-FTIR	Attenuated Total Reflectance-Fourier Transform Infrared Spectroscopy
d.m.b.	Dry matter basis
E.C.	Electrical Conductivity
EDX	Energy Dispersive X-ray
FA	Fulvic Acids
FESEM	Field Emission Scanning Electron Microscopy
HA	Humic Acids
HS	Humic Substances
NOM	Natural Organic Matter
SEC	Size Exclusion Chromatography
SS	Sewage Sludge
TOC	Total Organic Carbon
TS	Total solids
WWTP	Wastewater Treatment Plant

Wastewater production is rising all over the world as a consequence of the increasing population 47 and industrialization [1]. A recent study estimated that approximately 330 km³ of wastewater are 48 produced worldwide yearly [2]. For purification purposes, different treatment strategies can be 49 50 carried out, producing sewage sludge (SS) as the main by-product, which is stabilized mostly via anaerobic digestion [3]. A study by the European Commission revealed that Europe produces 17 kg 51 per capita of dry sludge per year [4]. SS is particularly rich in terms of plant nutrients, such as nitrogen 52 and phosphorous [5] and other beneficial compounds for good plant development, such as humic 53 54 substances [6]. Hence, agricultural reuse is the principal solution for SS disposal in many European countries, such as Portugal, Spain and the United Kingdom [7], as well as Chile and some other 55 Latin American states [8]. On the other hand, SS can retain many pollutants, such as heavy metals 56 57 [9]. Thus, the direct application of SS in soils can cause the accumulation of heavy metals in both 58 the soils and plants [10]. The extraction of humic substances (HS) is a potentially interesting strategy 59 to solve the problems associated with the presence of heavy metals and other undesirable 60 substances in SS.

HS are defined as the highly transformed part of non-living natural organic matter (NOM), which is 61 62 formed by organic compounds with structures that vary in their degree of complexity [11]. These substances are also defined as "the black gold of agriculture" [12] due to their beneficial effects on 63 soil quality and plant growth, a concept present in the literature for many years [13]. HS are natural 64 polymers with a highly heterogeneous structure and are traditionally classified as humic acids (HA), 65 fulvic acids (FA) and humins according to their solubility. In fact, FA are soluble at all pH, HA are 66 67 insoluble in acids, and humins are insoluble at all pH [14]. The molecular sizes range typically between 5 to 100 kDa for HA, and less than 10 kDa for FA [14, 15]. According to Grinhut and 68 69 colleagues [16], the half-life time of HS in nature can reach thousands of years, attributable mainly 70 to HA and humins, whose biodegradability is very slow. In sewage sludges from wastewater 71 treatment plants, HS are present in concentrations ranging from 7.7 to 28.6%, expressed as volatile 72 solids [17]. Typically, sludge HS are adsorbed to extracellular polymeric substances [18]. In particular, the distribution between HA and FA in sewage sludge varies between 24% and 76%, 73

depending on the characteristics of the wastewater as well as the operational conditions of the
wastewater treatment plant [[19], [20], [21], [22]].

76 The positive effects of HA on plant growth usually depend on many factors [23], such as the HA 77 concentration rate, plant species and origin of the raw material used as HA source. These effects include the improvement of the physico-chemical soil properties (such as water retention and soil 78 79 structure), and the increase of enzymatic activity and soil microbial diversity [24]. Moreover, Chen and Aviad [25] demonstrated that specific dosages of these substances can enhance seed 80 germination, stimulate root initiation and lateral root development, and boost root and shoot growth. 81 Many mechanisms are involved in plant growth and, amongst them all, the major role is mainly 82 attributed to the HA/plant membrane interaction. Indeed, improved performance membrane 83 transporters allow better absorption of soil nutrients [26]. A clear example is represented by 84 phosphorus bioavailability in soils treated with HA and P-fertilizer: HA increases water-soluble 85 phosphate, phosphorus plant uptake and plant biomass, retarding the formation of occluded 86 phosphate [27]. Hence, HA cannot replace mineral fertilizations, but they can provide more 87 productive cropping systems with fewer negative impacts on the environment deriving from the lower 88 89 application of fertilizers. All these characteristics consent HA to be used as biostimulants in horticulture [26]. Moreover, it is worth underlining that nowadays commercial HA derive mostly from 90 91 non-renewable resources, such as leonardite, coal and peat, while only in a few cases do they come 92 from renewable sources, such as compost and vermicompost [26].

93 Different biodegradable polymers have been studied as matrixes for the encapsulation of bioactive 94 compounds for different applications with the aim of having a controlled release of the substances 95 in time. The most used matrixes are chitosan, collagen, gelatin and alginate [[28], [29], [30]]. In the field of agriculture, different bioactive capsules can be found for the purpose of releasing herbicides 96 [31], fertilizers [32, 33], pesticides [34] or even complete cells that have a symbiotic effect with the 97 98 plant growth [35]. Generally, the objective of having a controlled release is to reduce the amount of 99 product that is added to the soil, which permits the operational costs to be reduced and, more importantly, ensures a constant and correct dose of each bioactive compound. As a consequence, 100

the product is not released into the environment, avoiding the environmental issues cited above.
 Another attractive feature of encapsulation is the reduction of bioactive compound deterioration.

103 Among the principal commercial polymers, alginate has the advantage of being a cost-effective 104 material, which is mainly extracted from brown algae. Alginate is a linear polysaccharide composed of two monosaccharide residues, (1,4)- β -D-mannuronic acid (M) and (1,4)- α -L-guluronic acid (G). 105 The particularity of alginate is that it can form a physical hydrogel (insoluble form) in the presence of 106 divalent cations such as Ca²⁺ and Ba²⁺, which form an ionic cross-linking between the G monomers 107 of two adjacent polymer chains [28]. The mechanism of the release of bioactive materials 108 encapsulated in alginate beads can be divided in two steps, the leakage of the bioactive compound 109 and the degradation of the matrix [30]. In fact, bioactive compounds with a size smaller than the 110 matrix pores are leached upon water irrigation, while the bigger ones are released after the 111 degradation of the matrix. The degradation occurs through alginate solubilization due to the action 112 of chelating compounds or extracellular enzymes. Chelators sequestrate the divalent cations yielding 113 to a disruption of the electrostatic interactions between the alginate chains and the Ca²⁺ cations. On 114 the other hand, enzymatic degradation is carried out by alginate lyases, which hydrolyze the 115 polysaccharide bonds. Thus, the degradation of alginate varies with the number of ionic bonds 116 between the Ca²⁺ and G monomers and will depend on the presence of microorganisms able to 117 produce alginate lyases enzymes in the soil [36]. 118

Adopting a circular economy approach, the principal aim of the present work was to evaluate the valorization of anaerobic sewage sludge from an agronomic point of view, with the purpose of improve soil quality. More in detail, a process of extraction of HA from ASS and their encapsulation in alginate beads was implemented to obtain an added-value product free from heavy metals and contaminants. The quality of the extracted HA was assessed with the size distribution analysis of the HA molecules and through electron microscopy. Finally, the effect of the HA beads on plant growth and biomass was evaluated on lettuce plants with a pot experiment under greenhouse conditions.

126 2. Materials and methods

127 2.1. Materials

Anaerobic sewage sludge (ASS) was sampled from a wastewater treatment plant (WWTP) in Chile.
Commercial HA, extracted from leonardite, were provided by Sanagro (Chile), Sodium alginate (food
grade) was purchased from Merck. All other chemicals used (KOH, K₄P₂O₇, HCl, NaOH, CaCl₂,
H₃BO₄, CuSO₄*H₂O, FeSO₄*7H₂O, MnSO₄*H₂O, NaMoO₄*2H₂O, ZnSO₄*7H₂O) were reagent-grade.
2.2. Extraction protocol

An extract of HA was obtained from ASS adapting the protocol of HS alkaline extraction from soil (Stevenson, 1994). The solid ASS was firstly mixed with water. Then KOH and $K_4P_2O_7$ was added in a ratio of 1:1 and the mixture was stirred at room temperature. The soluble part of the mixture was separated from the solids to obtain the HA extract.

137 2.3. Chemical analysis and HA quantification

Methods and results of chemical analysis of ASS are reported in **Supplementary material - 1**. Quantification of HA on ASS and HA extract was performed adapting the method proposed by Lamar and co-workers [37] on the analyzed matrixes. Quantification was carried out with the same method to the commercial HA as benchmark reference.

142 2.4. Molecular size distribution of HA

Membrane filtration was exploited to study molecular size distribution of humic acids in the HA 143 extract. To this aim, HA extract was submitted to three consecutive filtrations using membranes with 144 a progressively smaller cut-off. The membrane filtration process was designed as reported in **Fig. 1**, 145 146 using three different modules: i) filtration set-up with Buchner flask (aspired with vacuum pump) and Buchner funnel equipped with GF-6 filter paper (Merck-Millipore); ii) filtration set-up with Buchner 147 flask (aspired with vacuum pump) and Buchner funnel equipped with 0.45 µm membrane (Membrane 148 Solutions); iii) MilliporeSigma[™] Amicon[™] Bioseparations Stirred Cell (pressurized with N₂) equipped 149 with Ultracel 30 kDa (pore size $\simeq 6 - 7.5$ nm [38]), ultrafiltration disc (Merck Amicon Bioseparation). 150 151 Full technical details of filter membranes are provided in Fig. 1. After each filtration, filtrate was used partially for successive filtration, and partially for characterization of the filtrate. Characterization of 152 the filtrate included total solid analysis, HA quantification and measurement of total organic carbon 153 154 (TOC) with TOC analyzer (TOC-VWS, Shimadzu Corporation).

155 Figure 1 (in greyscale)

156 2.5. Encapsulation

157 The HS extract obtained from ASS was firstly sieved (0.8 mm) to remove residual debris. After that, 158 micronutrients were added to the solution in proportion inspired by Epstein and Bloom [39]. Concentration of these elements were: B 0.57 g L⁻¹, Cu 0.57 g L⁻¹, Fe 7.36 g L⁻¹, Mn 4.34 g L⁻¹, Mo 159 0.13 g L⁻¹ and Zn 1.12 g L⁻¹. After, the solution was mixed at 40°C with sodium alginate powder to a 160 final concentration of 2.3% w/v, until the solution resulted homogeneous. Hence, the mixture was 161 poured into a glass bottle and put under a nitrogen (N₂) pressure of 450 mbar to allow the injection 162 in the encapsulator Buchi B-390. The encapsulator was set at a frequency of 40 Hz and a voltage of 163 250 V. The solution extruded from the encapsulator was drop-shaped by a nozzle with a diameter of 164 1 mm. Drops fell in a hardening bath of CaCl₂ in the range of 0.06 - 6 M where the Na/Ca exchange 165 took place. Finally, beads were air dried. In order to measure diameters of dry and wet beads, beads 166 were photographed, and their pictures were analyzed with the ImageJ software [40]. 167

168 2.6. Microscopy analysis of extract and beads

With the purpose of describing morphological features of HA and evaluating the elements present in 169 the samples, the HA extract and alginate beads were investigated through Field Emission Scanning 170 Electron Microscopy (FESEM, Zeiss MERLIN, Gemini-II column, Oberkochen, Germany) and 171 Energy dispersive X-ray (EDX) analyses (AZTec, Oxford Instruments, Abingdon, UK). The EDX 172 analysis was performed on a wide area (100 µm x 100 µm) in three different regions of the samples 173 in order to have an average result of the elementary composition. Commercial HA were also 174 175 analyzed in order to get qualitative information on chemical composition and as a standard of comparison. Beads without HA were created and analyzed with FESEM in order to compare 176 structure of beads with HA and without. Previously all FESEM analysis, samples were metalized with 177 chromium. The liquid HA extract was previously dewatered to be analyzed by the means of FESEM. 178 179 Therefore, lyophilization was performed instead of classical thermal drying in order to not compromise the structure of HA. Lyophilization was performed with an IIShin FD5518 Freeze Dryer 180

with the following settings: temperature -60°C, pressure 5 mTorr, time 48 hours. As a result, a
lyophilized SA extract with 82% in dry matter was obtained.

183 2.7. ATR-FTIR spectroscopy

Lyophilized HA extract was analyzed by the means of Fourier transformed infrared (FTIR) spectroscopy, which was performed in attenuated total reflectance (ATR) mode. The instrument used was a Bruker Tensor 27 spectrometer equipped with a Platinum ATR and a KBr beamsplitter. The spectra were recorded in the range 4000-400 cm⁻¹ (mid IR) with a resolution of 4 cm⁻¹, 32 scans per sample (measurement time: 15 s) and background correction with ambient air.

189 2.8. Pot experiment

190 In order to evaluate beads effects on plant growth, a pot experiment was performed in a greenhouse located in Quillota, Valparaiso Region (Chile). Pots of 30 cm of diameter were filled with a sandy soil 191 previously sieved at 2.5 mm. Before the transplanting of Chilean lettuce plants (Lactuca sativa L.), a 192 193 basal dressing with a commercial NPK fertilizer for vegetables (N: 8%, P₂O₅: 15%, K₂O: 25%) and a 194 fungicide treatment with Captan (5 g L⁻¹) were applied in each pot following manufacturer 195 instructions. Three days after the transplanting, half of pots (9 replicates) were randomly treated with alginate-extract beads and the second half was no treated (control). The quantity of beads per-pot 196 was of 8.7 kg ha⁻¹ of HA due to a commercially recommended dosage as reported in the datasheet 197 198 of Humic plus®. A drip irrigation plant was installed, and plants were irrigated every 3 days. Finally, 199 70 days after transplanting, plants were cut at the basis, and epigean fresh biomass was immediately 200 weighted. Fresh biomass of root apparatus was measured after washing with water to remove residual soil particles. Finally, dry matter of the epigean and hypogean part of plants was weighted 201 202 after thermal treatment (105°C, 48 hours). Furthermore, chemical characterization of soils was 203 performed.

204 2.9. Statistical analysis

Data of the pot experiment were analyzed by one-way ANOVA (analysis of variance) with a Tukey's post-hoc test ($P \le 0.05$), after the assessment of the fundamental assumptions of ANOVA: the normality of distributions (Shapiro-Wilk test, p-value > 0.05) and the homogeneity of the variances of the residuals (Levene's test with P(>F) > 0.05). The statistical software R (version 3.5.1 - Feather Spray - 2018) was used for all statistical analysis.

210 3. Results and discussion

3.1. Quantification and characterization of HA

212 The application of the Lamar method [37] allowed the quantification of the HA content in ASS, HA extract and commercial HA. The results are summarized in Table 1. The HA content in ASS was 213 214 12.53 ± 1.60 % on dry matter basis (d.m.b.), a value comparable to other one reported in literature 215 (7.33%) [41]. The HA content in the extract was 26.87 ± 0.35% d.m.b., indicating that the process 216 contributed to a more than two-fold enrichment in HA. The quantification of the HA in commercial HA powder revealed the highest content, estimated in 77.87 ± 1.46% d.m.b., in line with other 217 commercial HA derived from leonardite (80%) [42]. Although the HA% of the extract is lower than 218 219 commercial HA, it is important to underline that normally HA are extracted from non-renewable resources, such as peat, lignite and leonardite, while in this case the HA came from a waste. 220

As regards membrane separation processes, it is worth specifying that this process was designed with two aims in mind. The first was the study of the molecular size distribution of the purified HS during extraction. The second was the individuation of one or more filters to separate HA from other components of the extract, with the purpose of increasing the purity and concentration of the final product.

As reported by Steelink [43], several techniques have been exploited to clarify the size and shape of 226 227 HA, such as sedimentation, size exclusion chromatography (SEC), light scattering and many others; however, each approach has pros and cons, revealing a broad range of molecular weight values. 228 Hence, the purpose of this study was not to investigate the theoretical molecular size distribution of 229 HA and their chemical moieties, as described by Shin and co-workers [44] for commercial HA. 230 231 Instead, the goal was to adopt an engineering approach which would permit a general 232 characterization, and at the same time would offer a potential process to obtain a more concentrated 233 product. For this reason, commercial membranes were used to design the filtration process. The

results of the membrane filtrations are reported in **Table 2**, which shows the concentrations of total
solids (TS), ashes, HA and TOC in the HA extract and the three permeates.

Considering that the HA extraction protocol did not reach extremely alkaline pH (9.5 - 10) to avoid 236 237 potential deterioration of HS, humins might still persist in the final extract (insoluble at pH>13 [45]. Furthermore, it must be taken into account that, even when extraction conditions are kept more 238 239 stringent, part of the non-humic organic material (e.g. cell material components) is solubilized and is 240 still present in the extract [45]. In the present study, these contributes were included in the quote of 241 humins and fulvic fraction (also known as "acid soluble fraction"), which is formed by FA and non-242 humic compounds [46]. In this study, TOC of the final extract is to be considered as consisting of 243 HA, fluvic fraction and humin fraction.

The content of HA, fluvic fraction and humin fraction in the different steps of the process where estimated from their mean elemental composition, with a C content of 55% for HA [47], of 50 % for fulvic fraction [48], and a 56 % for humins [49].

In parallel, Fig. 2 shows the distribution of the different components of the extract in function of the 247 different membrane pore size. On one hand, the first and second filtration process retained more 248 249 than a 40 % of TS and TOC, while HA and humin fraction were fully retained. Concerning humins, they were retained more by the first filter than the second one, according to their higher molecular 250 weights [50, 51]. Different is the case of HA, where researchers commonly agree that their molecular 251 weights ranges between 2 and 1300 kDa [52], which means that the estimated hydrodynamic radius 252 253 of HA particles varies between 2 [53] and 110 nm [54]. However, the literature has demonstrated 254 that HA may form aggregates with a mean particle diameter of 0.5 µm [11]. Thus, the results obtained with the membrane experiments suggested that HA molecules present in the extract formed 255 256 aggregates of different sizes, half bigger than 1 µm and half with a size included between 1 and 0.45 257 μm.

On the other hand, fluvic fraction and ashes were not affected by the filtration process and were present almost in its whole in the third permeate, which corresponded to the fraction with particle size smaller than 30 kDa. This indicated that they were mainly made of small inorganic molecules. In the case of ashes, they were likely made of elements such as potassium (as K⁺) and phosphorous (as PO₄³⁻) already present in ASS and further added during the extraction process, whose presence
 was confirmed by EDX analysis (see section 3.2).

Within the perspective to obtain an added-value product, the membrane processes yielded to an 264 265 increase in the concentration of HA, moving from a 26.87% w/w d.m.b. in the extract to a calculated value of 64% d.m.b summing the contributes of the first two filtration steps, which permitted to 266 accomplish successfully the full retention of HA. Therefore, the filtration in two steps, performed with 267 a 1 µm membrane followed by a 0.45 µm one, may be a feasible solution for the HA concentration. 268 269 In this context, the result of the present work indicated that the concentration and the increase in purification degree of HAs may be achieved with a microfiltration process, with smaller energy costs 270 271 than the ultrafiltration process proposed previously by Li and co-workers [55].

272

273 Table 1 (in greyscale)

- 274 Table 2 (in greyscale)
- 275 Figure 2 (in colors)

276 3.2. Encapsulation of HA extract in calcium alginate beads

The HA extract was encapsulated to obtain a solid product with a slow release of the active 277 components over time. Different concentrations of $CaCl_2$ (0.06 M – 6 M) were studied with the scope 278 279 of reducing the presence of Ca and Cl in the beads. However, concentrations below 0.6 M did not provide a solid formation of beads and therefore 0.6 M was chosen to harden the beads for pot 280 experiments. The beads were dried with the scope of increasing their lifetime by reducing the 281 possibility of microbial degradation, since they were mainly composed of organic matter [56]. After 282 one year of storage at 25°C in dry conditions, no visual damage neither degradation has been 283 284 observed. In addition, HA are known to be resistant to biodegradation, thus, the rate limiting step of release process can be reasonably attributed to the degradation of the alginate matrix [30]. The 285 286 mean diameter of wet and dry beads was 2.4 ± 0.4 mm and 1.1 ± 0.1 mm, respectively (from picture 287 analysis with ImageJ software). Considering that all the HA extract used during encapsulation was

successfully entrapped by beads, the content of HA in the dry beads represented the 6.09%,
according to the mass balance calculation.

290 Data from the literature report that Ca-alginate beads show macro-porous in the order of 10 µm [57] 291 and mesoporous in the range of 8 -14 nm [58]. This complex structure has been successfully used for the entrapment of complete cells on one hand, but on the other it has revealed enzymes leaching 292 [59]. Similarly to enzymes, HA can be washed out from the Ca-alginate matrix because of their 293 molecule size, which ranges between 2 and 1300 kDa [52]. However, as demonstrated by the 294 295 membrane process, the HA present in the extract formed aggregates bigger than 0.45 µm. This 296 result indicated that the aggregates were retained by the Ca-alginate matrix and that they would be released upon washing steps, (comparable to the effect of the irrigation process). 297

The FESEM images (**Fig. 3**) show the morphology of the surface of the beads, which was made of micrometer sized aggregates. Pure alginate structure is visible in **Fig. 3a**. The cluster of smaller globular particles that protrude from the entrapment made by the calcium alginate reticular structure, shown in **Fig. 3b**, confirmed the correct encapsulation of the HA extract within the calcium alginate matrix. A similar cluster-like structure is observed with the commercial HA (**Fig. 3d**). More compacted aggregates are observed from the lyophilized HA extract, which were due to the water elimination treatment (**Fig. 3c**).

305 The EDX analysis shown in Fig. 4 confirmed that the HA extraction process yielded to a product free of heavy metals. This was an interesting result, considering that the chemical analysis of the ASS 306 demonstrated the presence of As, Ni, Cd, Cr, Hg and Pb (Supplementary material - 1). Carbon, 307 308 nitrogen, and oxygen elements were not included in the EDX analysis because of the high errors associated with their low atomic weight. It is worth noting that the high standard deviation of the EDX 309 310 results obtained with the beads is in line with the FESEM images, which demonstrated the low homogeneity of the samples, showing regions with the presence of crystals and regions that are 311 clearer (Supplementary material - 2). The higher amount of K and P in the extract was attributed 312 to the use of a solution containing potassium hydroxide and pyrophosphate during the extraction 313 process. As expected, the content of these two components was considerably lower in the beads 314

due to the dilution of the extract in the alginate solution during beads preparation. In contrast, there was a substantial increase of sodium, chlorine and calcium in the beads with respect to the extract, which was in line with FESEM images showing crystals of NaCl on the beads surface (**Supplementary material - 2**). Those elements came from the sodium alginate and calcium chloride solution used to harden the beads. However, further washing steps to reduce the amount of the contaminants were not conducted in order to avoid the premature leaching of the HA molecules from the beads.

322 Figure 2 (print: in greyscale)

323 Figure 3 (print: in greyscale)

Infrared spectroscopy analysis of the lyophilized HA extract confirmed the presence of chemical 324 325 moieties peculiar of HS, as shown by Fig. 5, displaying ATR-FTIR absorption spectra with bands typical of HS. The sample spectra presented a principal band around 3270 cm⁻¹, corresponding to 326 327 the H-bonded O-H stretching of carboxylic acids, phenols, and alcohols and it was followed by a doublet at 2920-2850 cm⁻¹ due to the C-H stretching of aliphatic structures [[60], [61], [62], [63]]. 328 The peak around 1630 cm⁻¹ was ascribable to the C=O stretching of carboxylic and ketonic groups, 329 and to the aromatic C=C stretching [61, 63], followed by a peak around 1545 cm⁻¹ due to the C=N 330 stretching of amides [60, 61]. 331

Peaks at 1450 and 1400 cm⁻¹ were characteristic of the bending of aliphatic C-H and [60, 63] and of the O-H bending of carboxylic acid [64]. The large peak around 1040 cm⁻¹ corresponded to the C-O stretching of alcohols and aliphatic ethers [60], but it might be also assigned to the presence of Si–O silicate impurities as confirmed by EDX analysis [62, 63]. At lower wavelengths (900-600 cm⁻ ¹) the HA extract spectrum showed several peaks that could be reasonably attributed to the C=C bending [64]. ATR-FTIR spectra were recorded also on HA-alginate beads (data not shown), but the signal of alginate was too much intense, hindering the proper characterization of HA.

339 Figure 3 (in greyscale)

340 Figure 4 (in greyscale)

341 Figure 5 (in greyscale)

342 3.3. Pot experiment

343 The results of the final dry biomasses of lettuce grown in the greenhouse experiment are represented 344 in Fig. 6. As regards the epigean dry biomass of the lettuce plants, the addition of HA beads did not 345 provide significant differences with the untreated control. FESEM and EDX analyses (Fig. 3 and Fig. 346 4) showed NaCl presence in beads which probably contributed to the soil electrical conductivity (E.C.) of treated samples (0.46 dS m⁻¹) higher than control (0.26 dS m⁻¹) (**Supplementary material** 347 348 - 3). Nevertheless, E.C. did not reach potentially dangerous levels for plants (>2 dS m⁻¹) [65], and it 349 likely did not affect biomass production. Many studies about the effects on shoot biomass have been 350 conducted by adding HA to soils and the results are discordant. In some cases, no difference was reported, in others ones shoot biomass production was enhanced [26]. For studies dealing with 351 lettuce, no differences between treated and untreated samples were reported despite the high 352 353 amounts of HA applied (until 300 kg ha⁻¹) [66]. On the contrary, in another work lettuce plants had a statistically higher growth when compared to the untreated control at a dosage of 2000 mg of HA kg 354 ¹ of soil [67]. In the present work the estimated dosage of HA used was 8.7 kg ha⁻¹, corresponding 355 to approximately 2.7 mg of HA kg⁻¹ of soil, a dosage 740-fold lower than that reported in the work of 356 Tüfenkçi and colleagues [67]. On the other hand, in the present study the hypogean dry biomass of 357 358 plants grown in the presence of the HA beads was significantly higher (+63%) than the negative 359 control. Hence, this result confirmed the stimulation effect of HA on root growth, already widely documented in the literature [25, 26]. Moreover, this result supports the work of Young and Chen, 360 who demonstrated root biomass enhancement by HA in lettuce [68]. 361

It is important to underline that the enhancement of shoot biomass driven by HA addition to soil is more unusual. A work on tomato showed that only one out of nine dosages of HA applied promoted shoot biomass, but roots biomass production was promoted in all cases [69]. On the other hand, a recent meta-analysis of 89 papers on random-effects revealed that the dry weight of shoot and root increases of 22.4% and 21.6%, respectively, in response to HS application [23]. Furthermore, this study elucidated which are the significant factors likely enhancing shoots and roots growth using HS.

The type of HS (origin and chemical moieties) was the most important parameter in affecting both 368 369 shoots and roots biomasses increase. After that, the HS application rate resulted the most important parameter influencing shoot growth promotion, followed by stressing conditions and plant type. In 370 371 the present experiment, the not significant increase of shoot biomass could be due to some of these parameters but, as explained before, the low application rate was likely the most conceivable cause. 372 As regards root growth promotion, the above-mentioned study revealed that, after the HS type, the 373 growth media and plant species were the factors that mostly affected roots enhancement. Application 374 rate, application location and stress did not affect roots growth. In this way, our experiment 375 376 demonstrated that the HA extracted and applied to the plants were adequate to increase the biomass 377 of lettuce roots.

378 Figure 6 (in greyscale)

379 4. Conclusion

380 Sewage sludge is a waste with a high recycling potential considering its appreciable content in valuable compounds, but the simultaneous presence of toxic elements strongly limits its reuse. 381 382 Hence, an effective approach is the consideration of sewage sludge as a "raw material", candidate 383 to the selective "mining" of added value and profitable compounds. This strategy is in line with the purposes of the present work, which dealt with the extraction, quantification, characterization, and 384 agronomic testing of HA recovered from ASS. The protocol used allowed not only to obtain a HA 385 extract with a HA concentration (26.87%), on dry matter basis, doubled than the starting material 386 (ASS, 12.53%), but also to get rid of heavy metals. These positive results could be even more 387 388 improved with future research, optimizing the protocol for higher HA recovery. Membrane filtration, electron microscopy and infrared spectroscopy provided insight into peculiarities of HA extract, 389 revealing features on isolated HA comparable to those reported in the literature for what concerns 390 molecular sizes, morphology, and chemical moieties. The sequential filtration process permitted 391 392 determining that the extracted HA formed aggregates of size greater than 0.45 µm, making them suitable for encapsulation in alginate to obtain a slow release in soil. Despite the adequate 393 encapsulation of HA, NaCI was present in the capsules, but without affecting lettuce growth. In fact, 394

395 the HA-alginate beads induced beneficial effects on root apparatus growth of lettuce grown on a 396 poor and sandy soil (+63% over untreated control). With the purpose of further deepening these issues, future perspectives should include the testing of the effectiveness of other crosslinking 397 398 agents, to reduce NaCl content in beads, and the application of the slow-release HA product on different plant species. In conclusion, the encouraging results of this study suggest that HA extraction 399 from ASS is a promising strategy for the sustainable production of commercial HS of tomorrow. 400 Indeed, a slow-release bio-stimulant containing HA derived from a waste was achieved, successfully 401 402 fulfilling the circular economy principles.

403

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Parameter	Dry n	natter %	% HA (d.m.b.)		
Farameter	Mean value	Standard dev.	Mean value	Standard dev.	
ASS	25.58	± 0.49	12.53	± 1.60	
Extract	1.13	± 0.02	26.87	± 0.35	
Commercial HA	83.95	± 0.08	77.87	± 1.46	

Table 1. Dry matter mean percentages and humic acids mean percentages measured in anaerobic
sewage sludge (ASS), extract of SSAD (Extract) and commercial humic acids (Commercial HA).
d.m.b.: dry matter basis.

		Pure HA extract	GF-6 permeate	0.45 µm permeate	30 kDa permeate
	Dry matter (%)	1.13%	0.88%	0.64%	0.61%
	Total solids (g L ⁻¹)	10.7	8.32	6.03	5.74
Dry	vs pure extract	-	22.24%	43.64%	46.36%
matter	vs GF-6 filtrate	-	-	27.52%	31.01%
retention	vs 45 µm filtrate	-	-	-	4.81%
Ashes (dry	v matter basis) (g L-1)	4.52	4.50	4.39	4.30
	vs pure extract	-	0.54%	2.80%	4.87%
Ashes retention	vs GF-6 filtrate	-	-	2.27%	4.35%
Telefillon -	vs 45 µm filtrate	-	-	-	2.13%
Humic	acids (% dry matter)	26.87%	14.46%	n.a.	n.a.
	Humic acids (g L ⁻¹)	3.01	1.52	0	0
Humic	vs pure extract	-	49.50%	100.00%	100.00%
acids	vs GF-6 filtrate	-	-	100.00%	100.00%
retention	vs 45 µm filtrate	-	-	-	-
	TOC (g L ⁻¹)	3.32	2.02	0.81	0.71
	vs pure extract	-	39.16%	75.60%	78.61%
TOC retention	vs GF-6 filtrate	-	-	59.90%	64.85%
	vs 45 µm filtrate	-	-	-	12.35%

Table 2. Characterization of HA extract and filtrates from the three different filtration processes. Per

613 each parameter, percentages of retention are reported at each filtration step.

615 Figures

Fig. 1. Scheme of the membrane process exploited for study of molecular size of humic acids in the
extract based on membrane cut-off. Technical details are reported for each membrane.

Fig. 2. Retention percentages of total solids, ashes, humins, humic acids, fulvic fraction and total organic carbon along the different filtration steps.

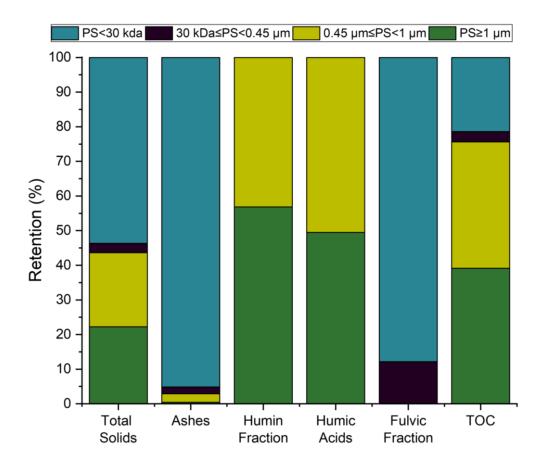
Fig. 3. FESEM images of the empty (a) and with HA extract (b) calcium alginate beads and of thelyophilized HA extract (c) and commercial HA powder (d).

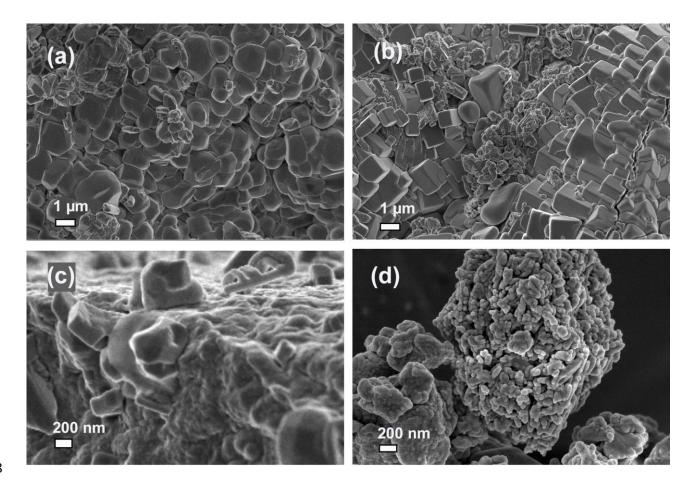
Fig. 4. Elementary composition by EDX analysis of the elements present in the samples of HA
extract, in commercial HA and in calcium alginate beads with HA.

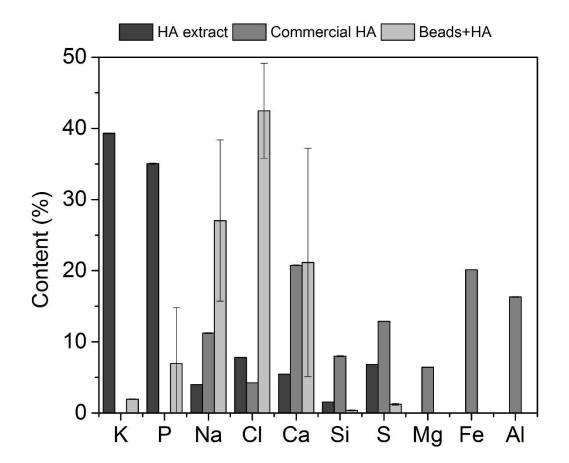
624 **Fig. 5.** ATR-FTIR spectrum of lyophilized HA extract.

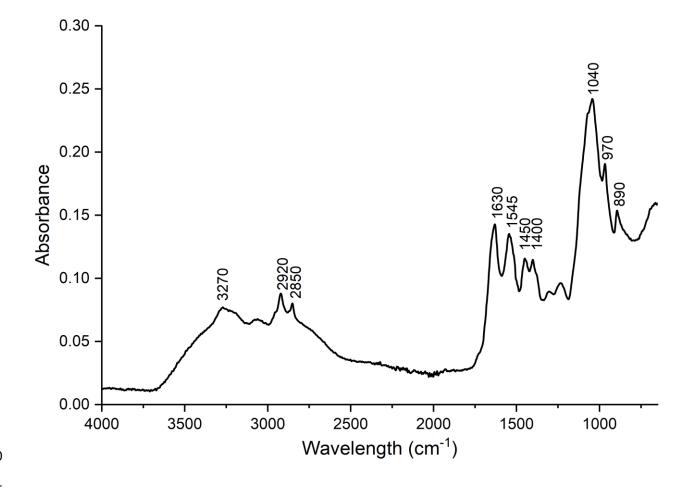
Fig. 6. Mean dry epigean and hypogean biomasses of *Lactuca sativa* L. grown on sandy soil with beads treatment and without beads treatment. Different letters indicate differences between treatments that are significant at P < 0.05 (Tukey HSD). Error bars represent standard error. Uppercase letters refer to statistical analysis applied to epigean dry biomass samples and lower-case letters refer to statistical analysis applied to hypogean dry biomass samples.

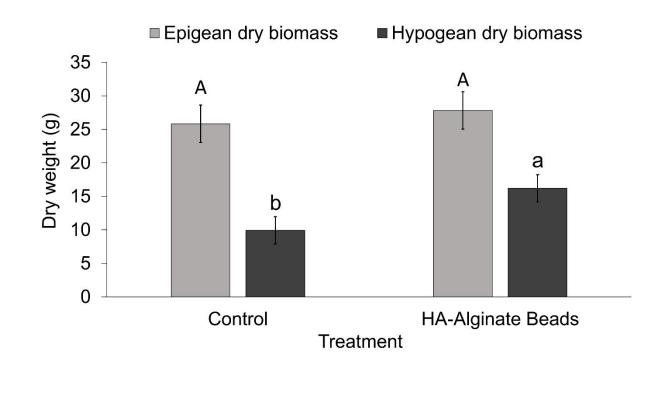
	Commercial name	ALMOST MERCENCE CONTRACTOR ALMOST	0.45 μm	Ultracel Ultrafiltration Disc
	Brand	Merck-Millipore	Membrane Solutions	Merck-Millipore
	Dimension	Ø 110 mm	Ø 47 mm	Ø 25 mm
	Cut-off	~ 1 µm	0.45 μm	30 kDa (6 ÷ 7.5 nm)
	Material	Paper/Glass Fiber	Mixed cellulose esters (MCE)	Regenerated cellulose
	Maximum flux	2.2 ml min ⁻¹	0.5 ml min⁻¹	0.17 ml min ⁻¹
	Pure HA Extract			
		GF-6 Filtrate	0.45 µm Filtrate ——	30 kDa Filtrate
	¥	¥	¥	¥
632	To quantification	To quantification	To quantification	To quantification
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