

1 **The ability of electrochemical oxidation with a BDD anode**
2 **to inactivate Gram-negative and Gram-positive bacteria in**
3 **low conductivity sulfate medium**

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14

15 **Abstract**

16 The disinfection of 100 mL of synthetic water containing 7 mM Na₂SO₄ with 10⁶ CFU mL⁻¹
17 of either Gram-negative or Gram-positive bacteria has been studied by electrochemical
18 oxidation. The electrolytic cell was a stirred tank reactor equipped with a boron-doped
19 diamond (BDD) anode and a stainless steel cathode and the trials were performed at acidic
20 and neutral pH, at 33 mA cm⁻² and 25 °C. Reactive oxygen species, pre-eminently hydroxyl
21 radicals, were efficiently produced in both media from water oxidation at the BDD anode and
22 the bacteria concentration was reduced by ≥ 5 log units after 60 min of electrolysis, thus
23 constituting a good chlorine-free disinfection treatment. All the inactivation kinetics were
24 described by a logistic model, with no significant statistical differences between acidic and
25 neutral suspensions. The electrochemical disinfection with BDD was very effective for Gram-
26 negative bacilli like *E. coli* and *P. aeruginosa* and Gram-positive ones like *B. atrophaeus*,
27 whereas the Gram-positive cocci *S. aureus* and *E. hirae* were more resistant. Thus, the latter
28 organisms are a better choice than *E. coli* as process indicators. Scanning electron microscopy
29 highlighted a transition from initial cells with standard morphology supported on clean filters
30 to inactivated cells with a highly altered morphology lying on dirty filters with plenty of
31 cellular debris. Larger damage was observed for Gram-negative cells compared to Gram-
32 positive ones. The inactivation effect could then be related to the chemical composition of the
33 outer layers of the cell structure along with the modification of the transmembrane potentials
34 upon current passage.

35 *Keywords:* *Bacillus atrophaeus*; Electrochemical disinfection; *Enterococcus hirae*;
36 *Escherichia coli*; *Pseudomonas aeruginosa*; *Staphylococcus aureus*

37

38 **1. Introduction**

39 The production of safe water in areas with increasing number of people and scarcity of
40 water is a need. Disinfection is used to reduce the number of pathogenic microorganisms to a
41 low enough level to ensure healthy conditions (WHO, 2015), and must prioritize
42 environmentally friendly methods. Chlorination is the most commonly used disinfection
43 procedure, but it entails several drawbacks such as Cl_2 accumulation and formation of
44 hazardous chloroderivatives. To solve these problems, other alternative methods including
45 ozonation, UV light irradiation and electrochemical disinfection have been developed
46 (Ghernaout and Ghernaout, 2010). To apply electrochemical disinfection as a green
47 technology, its effect on different types of microorganisms under controlled conditions has to
48 be tested.

49 Electrochemical advanced oxidation processes (EAOPs) have recently received
50 increasing attention for both, removal of organic pollutants from wastewater (Ciríaco et al.,
51 2009; Panizza and Cerisola, 2009; Sirés and Brillas, 2012; El-Ghenymy et al., 2014;
52 Martínez-Huitle et al. 2015) and disinfection of urban and industrial water (Kraft, 2008;
53 Cañizares et al., 2009; Rodrigo et al., 2010; Rajab et al.,2015; Werschkun et al., 2012),
54 including swimming pools (Nakajima et al., 2004). Electrochemical oxidation (EO) is the
55 most common EAOP utilized for electrochemical disinfection. It is characterized by easy and
56 mild operation conditions (Sirés et al., 2014) and possesses environmental compatibility due
57 to the in situ production of hydroxyl radical ($\cdot\text{OH}$) from water discharge at the anode surface,
58 without requiring the addition of noxious chemicals (Martínez-Huitle and Brillas, 2008;
59 Oturan et al., 2012; Thiam et al., 2015a, b). The most important parameters affecting the
60 disinfection process are the water composition, the hydrodynamics of the system, the kind of
61 anode material and the applied current density (j), since they determine the distribution of
62 oxidants and by-products (Mascia et al., 2012, 2013; Long et al., 2015). Metals like Pt

63 (Nakajima et al., 2004; Kerwick et al., 2005; Jeong et al., 2007; Delaedt et al., 2008), carbon
64 electrodes like graphite and activated carbon fiber (Shang et al., 2013), mixed metal oxides of
65 IrO₂, PbO₂, SnO₂, and/or TiO₂ (Martínez-Huitle and Brillas 2008; Panizza and Cerisola,
66 2008), and conductive boron-doped-diamond (BDD) (Furuta et al., 2004) have been used as
67 anodes. The BDD electrode has excellent properties including large resistance to corrosion in
68 very harsh media, large potential window, low adsorption of •OH and organics and higher O₂
69 overpotential than other anodes (Martínez-Huitle, 2007; Anglada et al., 2009; Sirés et al.,
70 2014). As a result, the BDD anode is considered the best one for EO, being able to mineralize
71 most organic molecules in sulfate medium (Hamza et al., 2009; Rodrigo et al., 2010; Pipi et
72 al., 2014; Scialdione et al., 2014).

73 It has been found that the direct electrolysis with conventional anodes such as Pt and
74 RuO₂ only yields a large disinfection when the treated liquid contains chloride ions (Polcaro
75 et al., 2007). This is due to the oxidation of Cl⁻ with formation of active chlorine species (Cl₂,
76 HClO and/or ClO⁻) that attack the bacterial cell. For example, Nakajima et al. (2004) reported
77 the inactivation of all tested bacteria in 5 min upon generation of 30 mg L⁻¹ active chlorine
78 using a Pt-Ir anode at 30 mA. In contrast, the BDD anode produces a more active •OH, highly
79 suitable for environmental application. The BDD anode is then very effective in the absence
80 of Cl⁻ ion, thus preventing the accumulation of active chlorine and the possible formation of
81 toxic organochlorinated products, chloramines, ClO₃⁻ and ClO₄⁻ (Vacca et al., 2013; Sirés et
82 al., 2014; Martínez-Huitle et al., 2015). In electrochemical disinfection, •OH is expected to
83 exhibit a superior inactivation performance compared to active chlorine because of its much
84 stronger oxidation ability (Cong et al., 2008). The most common supporting electrolyte to
85 investigate the role of •OH produced at BDD is Na₂SO₄, which presents enough conductivity,
86 maintains a correct osmotic potential for the bacterial cells and is chlorine-free.

87 Some bactericidal mechanisms have been proposed to explain the action of EO with
88 various electrodes under different experimental conditions. However, most of these studies
89 have been focused on *Escherichia coli* as process indicator and use chlorine-containing media
90 for the mediated oxidation by active chlorine (Drees et al., 2003; Kerwick et al., 2005; Jeong
91 et al. 2009). *E. coli* is an indicator microorganism for sanitary water quality and has been
92 widely used as a model organism due to its easy growth under laboratory conditions. Using a
93 BDD electrode in non-chloride media, Polcaro et al. (2007) reported a reduction of three
94 orders of magnitude of this bacterium in 60 s and Jeong et al. (2009) described an inactivation
95 of 2.4 log units in 3 min. In 0.10% Cl⁻ suspensions, Yao et al. (2011) found that the use of the
96 BDD anode was able to yield overall inactivation in a longer time of 30 min.

97 Other bacteria, with a different morphology and wall structure compared to *E. coli*,
98 should be comparatively tested in order to determine the actual disinfection ability of
99 electrochemical processes, as well as to validate *E. coli* as the right process indicator. To do
100 this, we have undertaken a study on the EO treatment of different Gram-positive and Gram-
101 negative strains that are the benchmark for the bactericidal tests according to the AENOR
102 standard.

103 This paper reports the results obtained for the electrochemical inactivation of five
104 bacteria with different cell walls and morphology, representatives of the bacterial pathogens
105 found in the aquatic environment. Two Gram-negative bacteria, *Escherichia coli* and
106 *Pseudomonas aeruginosa*, and three Gram-positive ones, *Bacillus atrophaeus*,
107 *Staphylococcus aureus* and *Enterococcus hirae*, were treated by EO with a BDD anode in
108 Na₂SO₄ medium under acidic and neutral conditions. The inactivation results of the five
109 organisms were modelled and compared to establish the most appropriate indicators for the
110 EO process. The changes in the outer structure of the cell walls were examined by scanning
111 electron spectroscopy (SEM).

112 2. Materials and methods

113 2.1. Tested bacteria and culture preparation

114 Strains of two rod-shaped Gram-negative bacteria, *Pseudomonas aeruginosa* ATTC
115 15442 and *Escherichia coli* ATTC 10536, one rod-shaped Gram-positive bacterium, *Bacillus*
116 *atrophaeus* ATCC 9372 (deposited as *B. subtilis* var. *niger*), and two Gram-positive cocci,
117 *Staphylococcus aureus* ATCC 6538 and *Enterococcus hirae* ATCC 10541, were used. The
118 bacteria were cultured in Trypticasein Soy Agar (TSA) plates, supplied by Laboratorio
119 Conda, at 37 °C for 24 h. Further, the cells were spiked in 2 mL of 7 mM Na₂SO₄ (analytical
120 grade from Panreac) and centrifuged at 14,000 rpm for 2 min. After washing twice with 1 mL
121 of 7 mM Na₂SO₄, the resulting pellet was resuspended in 1 mL of the same electrolyte giving
122 rise to an optical density at 600 nm (O.D. 600) of 0.7±0.1, corresponding to about 10⁸ colony-
123 forming units per mL (CFU mL⁻¹).

124 2.2. Electrolytic system

125 All the EO trials were performed in a one-compartment, two-electrode cylindric glass
126 tank reactor of 150 mL capacity. The cell was surrounded with a jacket to keep the treated
127 suspension at 25 °C under circulation of external thermostated water. The anode was a BDD
128 thin-film electrode purchased from NeoCoat and the cathode was a stainless steel (AISI 304)
129 sheet, both of 3 cm² area. The interelectrode gap was near 1 cm. Electrolytic trials were
130 carried out at a low constant current density of 33.3 mA cm⁻² to show the disinfection power
131 of EO with a BDD anode and under vigorous stirring with a magnetic bar at 800 rpm for
132 ensuring mixing and the transport of bacteria and cytoplasmic residues toward the anode.
133 Before the assays, the anode surface was cleaned via polarization in a 50 mM Na₂SO₄
134 solution at 100 mA cm⁻² for 180 min.

135 2.3. EO assays

136 For each disinfection experiment, 100 mL of aqueous solutions with 7 mM Na₂SO₄ were
137 prepared with ultrapure water of resistivity > 18 MΩ cm obtained from a Millipore Milli-Q
138 system. The solution was then spiked with a single bacterial strain (10⁸ CFU mL⁻¹) to obtain a
139 suspension with 10⁶ CFU mL⁻¹. The influence of pH on bacterial inactivation was studied at
140 acidic pH~3 by adding analytical grade H₂SO₄ from Panreac and at neutral pH~7 by adding
141 NaOH. The results were compared using the Kolmogorov-Smirnov statistical test.

142 After each treatment, the tank reactor was cleaned with 150 mL of a mixture composed of
143 100 mL of 33% (w/v) H₂O₂ (analytical grade from Panreac Química) and 100 ml of 96%
144 H₂SO₄ (analytical grade from Panreac Química) in 1 L of Milli-Q water for 10 min under
145 vigorous stirring. Afterwards, it was rinsed with ultrapure water and dried in an oven at 80 °C.
146 The electrodes were cleaned by immersion in ultrapure water at 100 °C for 10 min and,
147 subsequently, they were dried using an air stream.

148 *2.4. Instruments and analytical methods*

149 The O.D. 600 was measured with a Camspec M108 spectrophotometer. The pH and
150 electrical conductance of bacterial suspensions were determined with a Crison GLP 22 pH-
151 meter and a Metrohm 644 conductimeter, respectively. For electrolysis, the constant current
152 was provided by an Amel 2053 potentiostat-galvanostat, using a Demestres 601BR digital
153 multimeter for the instantaneous measurement of cell voltage. TOC analysis of samples
154 withdrawn from electrolyzed suspensions was carried out using a Shimadzu TOC-VCNS
155 analyzer. Reproducible TOC values with an accuracy of ±1% were found by injecting 50 μL
156 aliquots into the analyzer.

157 Aliquots of 1 mL were withdrawn at regular times for 60-90 min of electrolysis. These
158 samples were diluted and cultured in duplicate on TSA plates and incubated at 37 °C for 24 h.
159 Inactivation was determined from the reduction of culturability as log units reduction, i.e., log
160 (N_t/N_0), where N_t is the CFU value at given time and N_0 is the initial CFU value. The

161 theoretical detection limit was 1 bacterium per mL. All the EO trials were made thrice
162 (independent experiments).

163 The surface structure and morphological changes of each bacterium during EO
164 disinfection were analyzed by SEM (Gu et al., 2001; Diao et al., 2004). In each case, two
165 samples were collected at initial time and after 45 min of electrolysis. Each bacterial
166 suspension was filtered through a 0.2 μm polycarbonate membrane filter from Millipore. The
167 filter was then immersed for 30 min in a 2.5% glutaraldehyde solution buffered with 0.1 M
168 cacodylate at pH 7.4. Further, it was preserved at 4 $^{\circ}\text{C}$ before being processed as follows: The
169 filter was post-fixed in 1% OsO_4 , washed with 0.2 M sodium cacodylate and dehydrated with
170 a graded series of ethanol solutions from 30 to 100%, with 10% increments up to 80% and 5%
171 up to 100%. After dehydration, samples were dried with critical point drying and coated with
172 gold before observation. SEM images were obtained with a JEOL JSM-7001F equipment at
173 15 kV.

174 **3. Results and discussion**

175 *3.1. Operation conditions during EO disinfection*

176 The change in TOC, conductivity, cell voltage and pH for 100 mL of suspensions
177 containing 7 mM Na_2SO_4 and the single bacteria strains at a concentration of 10^6 CFU mL^{-1}
178 was determined after 60-90 min of EO treatment at 33.3 mA cm^{-2} to know the characteristics
179 of the disinfection process. TOC analysis is an alternative way to monitor the degradation of
180 the organic matter generated during the lysis of cells. An average TOC value of $2.55 \pm 1.50 \text{ mg}$
181 C L^{-1} was found for the initial bacterial suspensions, which arose from the bacteria content
182 plus compounds remaining upon culture preparation. TOC was only reduced to $2.25 \pm 0.90 \text{ mg}$
183 C L^{-1} in average at the end of EO. These findings point to a very small mineralization of the
184 organic matter, either the culture compounds or the spread cell wall and cytoplasm, during the

185 disinfection process. This suggests that the main action of the electric field and the $\bullet\text{OH}$
186 formed at the BDD surface during the electrolysis is the inactivation of the bacterial strains.
187 Similarly, the conductivity of $1.59\pm 0.1 \text{ mS cm}^{-1}$ of the untreated suspensions with 7 mM
188 Na_2SO_4 only increased slightly up to $1.70\pm 0.1 \text{ mS cm}^{-1}$, as expected if only small amounts of
189 cytoplasmic salts were released during the process. Regarding the average cell voltage of the
190 BDD/stainless steel tank reactor, it also underwent a small decay from $16.5\pm 1.6 \text{ V}$ to 15.8 ± 1.5
191 V during electrolysis, which can be related to the small increase in conductivity. In the case of
192 solution pH, no significant variation was observed during the EO treatments. Thus, the pH of
193 acidic solutions varied from 3.2 ± 0.3 to 3.4 ± 0.5 , whereas the pH of neutral solutions changed
194 from 7.1 ± 0.2 to 7.6 ± 0.6 . This indicates that, under our experimental conditions with an
195 undivided tank reactor, the H^+ formation from water oxidation at the BDD anode was
196 counterbalanced either by its reduction at the cathode under acidic conditions or,
197 preferentially, by OH^- production at the cathode in neutral medium (Cho et al., 2004; Sirés et
198 al., 2014).

199 All the aforementioned results bring to consider that the EO treatments of all bacteria
200 suspensions occurred under quasi-steady conditions and thus, the main effects were at cellular
201 and subcellular level but did not alter the macroscopic properties of the suspensions.

202 3.2. Effect of pH on bacteria inactivation

203 A first series of experiments was carried out to assess the stability of the different bacteria
204 in suspensions at pH near 3 and 7 before EO treatment. The acidic medium was chosen to
205 further check in future the viability of other EAOPs like electro-Fenton and photoelectro-
206 Fenton that operate at optimum pH close to 3 (Sirés and Brillas, 2012; Thiam et al., 2015c).
207 The two Gram-negative microorganisms, *P. aeruginosa* and *E. coli*, as well as the Gram-
208 positive cocci *S. aureus* and *E. hirae*, did not undergo any kind of inactivation in the two
209 tested media. In contrast, the content of the Gram-positive bacterium *B. atrophaeus* was not

210 stable in none of the sulfate media since it was reduced by two log units at pH~3 and half log
211 unit at pH~7 after 60 min of stirring. Note that Geveke and Kozempel (2003) have also
212 reported that acidification of *E.coli* suspensions did not cause any inactivation of this
213 bacterium.

214 According to the above results, the suspensions of all the bacteria in 7 mM Na₂SO₄ were
215 prepared just before their EO treatment at 33.3 mA cm⁻² to obtain comparable inactivation
216 data. Fig. 1 depicts the gradual reduction of log (N_t/N_0) with electrolysis time for the five
217 bacteria in the two tested media. As can be seen, the content of all strains diminished more
218 than 5 log units upon electrolysis, although with different inactivation kinetics.

219 Fig. 1 shows that the inactivation was already quantitative at 45 min, since at pH~3 the
220 log (N_t/N_0) values of all the bacteria diminished about 6 units, except in the case of *E. hirae*
221 since it decayed near 5 log units. Similarly, the results at pH~7 showed that the rod-shape
222 bacteria decreased 6 log units or more, whereas the cocci dropped about 4.5 log units. At the
223 end of the EO treatment, Fig. 1 evidences that the two Gram-negative as well as the Gram-
224 positive bacilli were totally inactivated, whereas in the case of Gram-positive cocci, *S. aureus*
225 and *E. hirae*, some few cells still survived, except in the case of *S. aureus* at pH~3. Despite
226 the differences observed for the electrochemical disinfection at pH near 3 and 7, it can be
227 concluded that the effect of pH was not statistically significant according to the Kolmogorov-
228 Smirnov test, as will be discussed below.

229 The five strains suspended in synthetic water with 7 mM Na₂SO₄ at both pH values tested
230 then showed a reduction of ≥ 5 log (N_t/N_0) units in 60 min by EO with a BDD anode at a
231 current density of 33.3 mA cm⁻². This significant bacterial inactivation, greater than 99.999%,
232 was mainly achieved by the action of the physisorbed BDD([•]OH) radicals formed at the BDD
233 surface from the anodic oxidation of water (Martínez-Huitle and Brillas, 2008; Panizza and
234 Cerisola, 2009). Under comparable conditions, our results highlight that the most resistant

235 bacteria were the cocci *S. aureus* and *E. hirae*, whereas the most fragile microorganism was
236 the bacillus *B. atrophaeus*, being all Gram-positive. Based on the electrochemical inactivation
237 found, one can divide the tested bacteria into three groups:

238 (i) The two Gram-negative bacilli, *E. coli* and *P. aeruginosa*, with a very similar
239 inactivation rate.

240 (ii) The two Gram-positive cocci, *S. aureus* and *E. hirae*, which were the most resistant
241 microorganisms to this kind of treatment, and

242 (iii) finally, the Gram-positive bacillum, *B. atrophaeus*, which was the most fragile,
243 which can be at least partly linked to its sensitivity to pH variations during EO.

244 It should be noted that *B. atrophaeus* has been called *B. subtilis var. niger* in previously
245 published literature and, consequently, much information about its inactivation is given
246 elsewhere, especially when it is in its sporulated form that largely increases its resistance
247 (Yoon et al., 2007). However, when survival studies were performed with vegetative cells, as
248 in our case (disinfection is only related to vegetative forms), it has simply been reported that
249 *B. subtilis* declined more rapidly than other Gram-positive bacteria like *P. fluorescens* in soils
250 (Van Elsas et al., 1986).

251 Other authors have also compared the inactivation of several bacteria by EO with a BDD
252 anode, showing similar trends to those found by us. Thus, Polcaro et al. (2007) reported a
253 reduction of the content of *E. coli*, coliforms and enterococci from 10^3 CFU mL⁻¹ to their
254 detection limit after 60, 100 and 300 s of electrolysis, respectively, using 1 mM Na₂SO₄ at 10
255 mA cm⁻². On the other hand, Heim et al. (2015) described fast bacterial reduction rates, close
256 to 5 log units, for *E. coli*, *P. aeruginosa* and *E. faecium* up to a specific charge consumption
257 of 75 mAh L⁻¹, followed by a continuous but much slower inactivation.

258 It must be mentioned that, apart from the strong physisorbed oxidant BDD([•]OH)
259 generated at the BDD surface, this anode can also form other weaker reactive oxygen species

260 (ROS) from water oxidation such as atomic oxygen ($\cdot\text{O}$), H_2O_2 and O_3 (Polcaro et al., 2007;
261 Martínez-Huitle and Brillias, 2008). Furthermore, other weaker oxidants can be produced from
262 the oxidation of the supporting electrolyte, like persulfate ($\text{S}_2\text{O}_8^{2-}$) ion from the oxidation of
263 SO_4^{2-} ion (Sirés et al., 2014). All these oxidizing species are helpful for disinfection because
264 they can damage the cell membranes, therefore altering their permeability and finally leading
265 to their rupture (Diao et al., 2004). This point will be discussed below from SEM analysis of
266 the untreated and inactivated bacteria.

267 3.3. Modelling inactivation kinetics

268 Numerous models have been proposed to describe bacterial survival curves, some of
269 them including terms that account for shoulder and tailing phenomena. The logarithmic
270 inactivation data for each bacteria shown in Fig. 1 were adjusted to a modified logistic model
271 based on Kamau et al. (1990), expressed as follows:

$$272 \log(N_t/N_0) = \frac{I}{1 + a \exp(i t)} \quad (1)$$

273 where I denotes the theoretical maximum log reduction achieved upon the EO treatment, a is
274 a parameter of adjustment related to the shape of the first shoulder, i is the inactivation rate (in
275 min^{-1}) and t is the electrolysis time (in min). It should be mentioned that ideal mixing is
276 assumed here, thus ensuring the maximum mass transport toward/from the electrodes.
277 Therefore, the existence of poor hydrodynamic conditions in our laboratory cell can be
278 discarded. In contrast, Mascia et al. (2012) reported the significant effect of flow pattern
279 inside the disinfection unit when treating larger volumes using a filter-press cell, owing to the
280 dispersion phenomena, stagnant zones and bypass flows. When Eq. (1) was applied, it was
281 observed that the second shoulder or tail was highly influenced by the detection limit of the
282 processed volume and the initial concentration of the studied bacteria. Since the fittings were
283 very similar at pH close to 3 and 7, a unique pH-independent plot has been represented from

284 the independent trials made for each bacterium. Fig. 2a-e depicts the graphs thus obtained for
285 the five bacteria, along with the corresponding curves (upper and lower dashed lines) related
286 to 95% confidence intervals on these fits. Table 1 summarizes the fitting parameters of Eq. (1)
287 found in each case, along with the square of their regression coefficients (R^2). The latter
288 values corroborate the goodness of Eq. (1) to describe the inactivation trends of all the tested
289 bacteria.

290 As expected, a first look to Fig. 2 confirms that *S. aureus* was the most resistant strain,
291 whereas *B. atrophaeus* was the most sensitive one. No significant differences can be observed
292 between the intermediate inactivation values of the other bacteria. For example, *S. aureus*
293 reached a 4 log reduction after 38 min of EO treatment, whereas 30 min were required for *E.*
294 *coli*, 28 min for *P. aeruginosa*, 23 min for *E. hirae* and only 14 min for *B. atrophaeus*. Total
295 inactivation of the latter one with a decrease of 6 log units was already reached in 30 min. A
296 similar drop of more than 6 log units for *E. coli* and *P. aeruginosa* was found after 60 min of
297 electrolysis, whereas *S. aureus* and *E. hirae* required longer time to attain their total
298 inactivation. For *E. coli*, *P. aeruginosa*, *S. aureus* and *E. hirae*, a first shoulder at short time
299 can be seen in Fig. 2a, b, d and e, respectively, whereupon the $\log(N_t/N_0)$ values decayed up
300 to reach overall disinfection, although for *E. hirae*, the inactivation rate seemed to become
301 drastically reduced once reached a 5 log reduction. The presence of the initial shoulder could
302 be related with the existence of more resistant cells within the whole bacteria populations.
303 This trend was not valid for *B. atrophaeus*, which underwent a much quicker inactivation
304 from the beginning of the electrolysis. Therefore, the classification mentioned in Section 3.2
305 is now verified:

306 (i) The two Gram-negative bacilli, *E. coli* and *P. aeruginosa*, presented a first shoulder in
307 the $\log(N_t/N_0)$ -t plot, followed by a rapid steep decay to end in their total inactivation.

308 (ii) The two Gram-positive cocci, *S. aureus* and *E. hirae*, presented a first shoulder in the
309 $\log(N/N_0)$ - t plot as well, followed by a less pronounced drop than in case (i) to end in a tail.
310 This behavior evidences the need of longer time to reach their total inactivation, and

311 (iii) finally, the Gram-positive bacillum, *B. atrophaeus*, was rapidly inactivated with no
312 shoulder appearing during the treatment.

313 To better compare the EO disinfection of bacterial suspensions, the times for 1 log
314 reduction or 90% of inactivation ratio (T_{90}), 2 log or 99% (T_{99}), 3 log or 99.9% ($T_{99.9}$), 4 log or
315 99.99% ($T_{99.99}$) and 5 log or 99.999% ($T_{99.999}$) were determined considering the kinetic
316 relationship given by Eq. (1). The data obtained are summarized in Table 2. As can be seen,
317 *B. atrophaeus*, a rod-shaped Gram-positive bacterium, required shorter times for inactivation
318 compared to the others, regardless of the considered inactivation ratio. For both rod-shaped
319 Gram-negative bacteria, *P. aeruginosa* and *E. coli*, $T_{99.99}$ was between 28 and 30 min and
320 $T_{99.999}$ between 32 and 35 min. In contrast, the Gram-positive cocci needed longer times to
321 reach a given inactivation ratio, in agreement with their higher resistance. While in the case of
322 *E. hirae*, $T_{99.99}$ was similar to that found for Gram-negative bacteria, *S. aureus* presented a
323 higher value. As for $T_{99.999}$ values, the difference was larger than 11 and 27 min compared to
324 the Gram-negative and Gram-positive bacilli, respectively. For example, the differences
325 between *E. coli* and *S. aureus* were of 7 and 11 min for $T_{99.99}$ and $T_{99.999}$, respectively, and up
326 to 23 and 27 min in the case of *B. atrophaeus* vs. *S. aureus* to reach those inactivation ratios.

327 Interestingly, once reached an inactivation ratio of 90%, the three bacilli, *E. coli*, *P.*
328 *aeruginosa* and *B. atrophaeus*, needed similar time intervals to ensure an additional log unit
329 reduction, ranging between 3.1 and 4.8 min, whereas *S. aureus* required longer intervals
330 (between 5.8 and 8.2 min). In the case of *E. hirae*, the time intervals up to $T_{99.9}$ were similar to
331 those of bacilli (3.1 - 4.8 min), but from $T_{99.99}$ to $T_{99.999}$ the intervals became longer, being
332 analogous to those of *S. aureus*. For most bacteria, the time intervals between T_{99} and $T_{99.9}$ and

333 between $T_{99,9}$ and $T_{99,99}$ were then shorter than the initial interval from T_{90} to T_{99} and the last
334 interval to $T_{99,999}$. This behavior was also verified for *E. hirae* but only up to $T_{99,9}$.

335 Our results agree with those from other authors that pointed out that, in general, big cells
336 tend to be more susceptible to an electric field than small and oval ones, which may justify the
337 significantly slower inactivation of cocci compared to bacilli (Machado et al., 2010;
338 Guillemes Peira, 2014). On the other hand, it has been reported that the Gram-negative
339 bacteria are more sensitive than the Gram-positive ones to pulsed electric fields (Barsotti and
340 Cheftel, 1999; Jeyamkondan et al., 1999). This has also been found in the present study,
341 except in the case of *B. atrophaeus*.

342 3.4. SEM analysis during disinfection trials

343 SEM micrographs of the cells of the different bacterial strains were obtained before
344 electrolysis and after 45 min of their EO treatments with a BDD anode at 33.3 mA cm^{-2} , as
345 depicted in Fig. 3a-e. Before treatment, the cells showed their standard morphology, three
346 bacillary forms of similar size and two coccoid forms, and the filters were clean. In contrast,
347 their morphology was largely altered upon EO disinfection, becoming the cell surface of all
348 the bacteria much rougher. Moreover, the filters became dirty with a great deal of cellular
349 debris, probably because large amounts of cellular material were released from the inactivated
350 cells. *E. coli* (see Fig. 3a) and *P. aeruginosa* (see Fig. 3b), both with a Gram-negative cell
351 wall, underwent the most significant surface modification, which was less evident in the case
352 of the bacteria with a Gram-positive wall, like the bacillus *B. atrophaeus* (see Fig. 3c) and the
353 cocci *S. aureus* (see Fig. 3d) and *E. hirae* (see Fig. 3e). However, it seems that the cell
354 appearance of the latter two organisms pointed to some shrinkage.

355 The inactivation kinetics of the tested strains and their morphological changes can then be
356 related to the attack of ROS, like BDD($\bullet\text{OH}$) and O_3 , produced in situ by EO on their cellular
357 walls having different structure. The effect of these oxidants can be explained from other

358 disinfection techniques. It has been described that they diffuse toward the outer layers of the
359 bacterial cells and then infiltrate into the membrane and cytoplasm, reacting with proteins and
360 unsaturated lipids. Consequently, the cell walls may be broken by lysis, causing the leakage
361 of inner compounds to the reaction medium and, simultaneously, the radicals can penetrate
362 into the cytoplasm and affect the enzymes and DNA molecules (Hunt and Mariñas, 1999).
363 Accordingly, our SEM results show that the ROS generated by BDD caused changes in the
364 cell envelope, which became rougher, especially in the Gram-negative bacilli. The vast
365 majority of the cells, after 45 min of electrolysis, lost their growth ability, despite the
366 apparently unaffected morphology of most of them, as also claimed by other authors
367 (Machado et al., 2010). Hunt and Mariñas (1999) explained that chemical reactions between
368 O₃ and biomolecules continue after loss of inactivation until the disinfectant is exhausted or
369 the biomolecules are completely oxidized. Thus, the generated ROS in EO directly affect the
370 cell walls causing their membrane cleavage (Diao et al., 2004). Other authors have also
371 reported that the EO treatment of *E. coli* in sulfate medium induces damage to the cell
372 membrane. The generated chemicals attack the membrane proteins and modify the K⁺
373 balances, which affects the cell division and the synthesis of cellular ATP until causing the
374 bacterial inactivation (Polcaro et al, 2007, Jeong et al., 2009). Long et al. (2015) also
375 observed lipid peroxidation during electrochemical disinfection with a BDD anode.

376 According to our SEM observations, bacteria with Gram-positive wall preserve their cell
377 structure better than the Gram-negative ones. This could be explained by the molecular
378 composition of the outer layers, since the Gram-positive cells have a thick peptidoglycan
379 layer, whereas the Gram-negative ones only have a phospholipid bilayer with
380 lipopolysaccharide molecules and proteins under which there is a much thinner peptidoglycan
381 layer. Some studies have shown that the phospholipid membrane is hardly oxidizable,
382 whereas the proteins are easier to destroy under the direct effect of the electric current (Linley

383 et al., 2012). There is less information about the relationship between ROS and the outer
384 membrane of Gram-positive cells, but our results suggest that their outer layer was quite
385 resistant during inactivation, maintaining the initial structure despite the slight size reduction
386 observed in the case of both cocci. It is also noteworthy that electrogenerated H_2O_2 and O_3
387 can go through the membranes and reach the vital centre of the cells (Drogui et al., 2001)

388 An additional significant difference observed upon EO treatment was the appearance of
389 cellular debris, also described elsewhere. For example, Diao et al. (2004) observed substantial
390 intracellular materials leaked out from the cells after electrochemical disinfection of *E. coli*
391 suspensions using dimensionally stable anodes, which was ascribed to the oxidation of the
392 membranes by electrogenerated ROS such as peroxides, $\bullet\text{OH}$ and ozone. Finally, note that in
393 the EO assays the cell membranes might undergo large modifications of their transmembrane
394 potentials due to the concomitant electric field of ca. 16.5 V cm^{-1} in the BDD/stainless steel
395 tank reactor. It has been reported that, if the resulting transmembrane potential value ranges
396 between 0.2 and 1 V, reversible pore formation in the membrane (electroporation or
397 electropermeabilization) may occur. Greater values lead to the cell death (Weaver and
398 Chizmadzhev, 1996; Machado et al., 2010), therefore contributing to their inactivation. Since
399 critical electric fields in the kV cm^{-1} range would be necessary to promote irreversible
400 electroporation (García et al., 2016), its contribution in the present study seems rather
401 insignificant.

402 **4. Conclusions**

403 It has been shown that the five tested bacterial strains, two Gram-negative and three
404 Gram-positive, suspended at 10^6 CFU mL^{-1} in synthetic water with 7 mM Na_2SO_4 ,
405 experienced a significant reduction of at least 5 log units within 60 min of EO with a BDD
406 anode at 33.3 mA cm^{-2} . This method can then be considered a suitable chlorine-free

407 disinfection treatment. ROS, pre-eminently hydroxyl radicals, generated at the BDD surface
408 were very efficient under acidic and neutral conditions. Although apparently the inactivation
409 seemed more effective at pH~3, no relevant statistical differences were found at pH~7. A
410 modified logistic model has been used to describe the inactivation kinetics in all cases. The
411 electrochemical disinfection with BDD was very effective for the bacilli *E. coli*, *P.*
412 *aeruginosa* and *B. atrophaeus*, being the latter one much more sensitive. In contrast, the
413 Gram-positive cocci *S. aureus* and *E. hirae* were more resistant and, consequently, they
414 should be chosen as more appropriate indicators than *E. coli* for the EO treatment. The SEM
415 micrographs of all bacteria showed a transition from cells with standard morphology
416 supported on clean filters to cells with a highly altered morphology lying on dirty filters with
417 plenty of cellular debris due to their lysis. These observations revealed a greater damage in
418 the case of the Gram-negative organisms, due to their particular cell wall structure. The
419 overall inactivation effect can then be explained not only on the basis of oxidizing
420 electrogenerated ROS but also from the different chemical composition of the outer cell
421 layers and the large modifications of the transmembrane potentials upon application of the
422 electric current.

423 **Acknowledgements**

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428 **References**

429 Anglada, A., Urtiaga, A., Ortiz, I., 2009. Contributions of electrochemical oxidation to waste-

430 water treatment: Fundamentals and review of applications. *J. Chem. Technol. Biotech.*
431 84(12), 1747–1755.

432 Barsotti, L., Cheftel, J.C., 1999. Food processing by pulsed electric fields. II. Biological
433 aspects. *Food Rev. Int.* 15(2), 181–213.

434 Cañizares, P., Hernández, M., Rodrigo, M.A., Saez, C., Barrera, C.E., Roa, G., 2009.
435 Electrooxidation of brown-colored molasses wastewater. Effect of the electrolyte salt on
436 the process efficiency. *Ind. Eng. Chem. Res.* 48(3), 1298–1301.

437 Cho, M., Chung, H., Choi, W., Yoon, J., 2004. Linear correlation between inactivation of *E.*
438 *coli* and OH radical concentration in TiO₂ photocatalytic disinfection. *Water Res.* 38(4),
439 1069–1077.

440 Ciríaco, L., Anjo, C., Correia, J., Pacheco, M.J., Lopes, A., 2009. Electrochemical
441 degradation of ibuprofen on Ti/Pt/PbO₂ and Si/BDD electrodes. *Electrochim. Acta*
442 54(5), 1464–1472.

443 Cong, Y., Wu, Z., Li, Y., 2008. Electrochemical inactivation of coliforms by in-situ generated
444 hydroxyl radicals. *Korean J. Chem. Eng.* 25(4), 727–731.

445 Delaedt, Y., Daneels, A., Declerk, P., Behets, J., Ryckeboer, J., Peters, E., Ollevier, F., 2008.
446 The impact of electrochemical disinfection on *Escherichia coli* and *Legionella*
447 *pneumophila* in tap water. *Microbiol. Res.* 163(2), 192–199.

448 Diao, H.F., Li, X.Y., Gu, J.D., Shi, H.C., Xie, Z.M., 2004. Electron microscopic investigation
449 of the bactericidal action of electrochemical disinfection in comparison with
450 chlorination, ozonation and Fenton reaction. *Process Biochem.* 39(11), 1421–1426.

451 Drees, K.P., Abbaszadegan, M., Maier, R.M., 2003. Comparative electrochemical inactivation
452 of bacteria and bacteriophage. *Water Res.* 37(10), 2291–2300.

453 Drogui, P., Elmaleh, S., Rumeau, M., Bernard, C., Rambaud, A., 2001. Oxidising and
454 disinfecting by hydrogen peroxide produced in a two-electrode cell. *Water Res.* 35(13),
455 3235-3241.

456 El-Ghenymy, A., Centellas, F., Garrido, J.A., Rodríguez, R.M., Sirés, I., Cabot, P.L., Brillas,
457 E., 2014. Decolorization and mineralization of Orange G azo dye solutions by anodic
458 oxidation with a boron-doped diamond anode in divided and undivided tank reactors.
459 *Electrochim. Acta* 130, 568–576.

460 Furuta, T., Tanaka, H., Nishiki, Y., Pupunat, L., Haenni, W., Rychen, Ph., 2004. Legionella
461 inactivation with diamond electrodes. *Diam. Rel. Mater.* 13(11-12), 2016–2019.

462 García, P.A., Ge, Z., Moran, J.L., Buie, C.R., 2016. Microfluidic screening of electric fields
463 for electroporation. *Sci. Rep.* 6, 21238.

464 Geveke, D.J., Kozempel, M.F., 2003. Pulsed electric field effects on bacteria and yeast cells.
465 *J. Food Process. Preserv.* 27(1), 65–72.

466 Ghernaout, D., Ghernaout, B., 2010. From chemical disinfection to electrodisinfection: The
467 obligatory itinerary? *Desalin. Water Treat.* 16(1-3), 156–175.

468 Gu, J., Belay, B., Mitchell, R., 2001. Protection of catheter surfaces from adhesion of
469 *Pseudomonas aeruginosa* by a combination of silver ions and lectins. *World J.*
470 *Microbiol. Biotechnol.* 17(2), 173–179.

471 Guillemes Peira, A., 2014. Aplicación de la oxidación avanzada en la desinfección de aguas
472 residuales. *Ing. Hidráulica Ambiental* 35(3), 60–72.

473 Hamza, M., Abdelhedi, R., Brillas, E., Sirés, I., 2009. Comparative electrochemical
474 degradation of the triphenylmethane dye Methyl Violet with boron-doped diamond and
475 Pt anodes. *J. Electroanal. Chem.* 627 (1-2), 41-50.

476 Heim, C., Ureña de Vivanco, M., Rajab, M., Müller, E., Letzel, T., Helmreich, B., 2015.
477 Rapid inactivation of waterborne bacteria using boron-doped diamond electrodes. *Int. J.*

478 Environ. Sci. Technol. 12(10), 3061–3070.

479 Hunt, N.K., Mariñas, B.J., 1999. Inactivation of *Escherichia coli* with ozone: chemical and
480 inactivation kinetics. *Water Res.* 33(11), 2633-2641.

481 Jeong, J., Kim, J.Y., Cho, M., Choi, W., Yoon, J., 2007. Inactivation of *Escherichia coli* in
482 the electrochemical disinfection process using a Pt anode. *Chemosphere* 67(4), 652–
483 659.

484 Jeong, J., Kim, C., Yoon, J., 2009. The effect of electrode material on the generation of
485 oxidants and microbial inactivation in the electrochemical disinfection processes. *Water*
486 *Res.* 43(4), 895–901.

487 Jeyamkondan, S., Jayas, D.S., Holley, R.A., 1999. Pulsed electric field processing of foods: A
488 Review. *J. Food Prot.* 62(9), 1088–1096.

489 Kamau, D.N., Doores, S., Pruitt, K.M., 1990. Enhanced thermal destruction of *Listeria*
490 *monocytogenes* and *Staphylococcus aureus* by the lactoperoxidase system. *Appl.*
491 *Environ. Microbiol.* 56(9), 2711–2716.

492 Kerwick, M.I., Reddy, S.M., Chamberlain, A.H.L., Holt, D.M., 2005. Electrochemical
493 disinfection, an environmentally acceptable method of drinking water disinfection?
494 *Electrochim. Acta* 50(25-26), 5270–5277.

495 Kraft, A., 2008. Electrochemical water disinfection: A short review. *Platin. Met. Rev.* 52(3),
496 177–185.

497 Linley, E., Denyer, S.P., McDonnell, G., Simons, C., Maillard, J.Y., 2012. Use of hydrogen
498 peroxide as a biocide: new consideration of its mechanisms of biocidal action. *J.*
499 *Antimicrob. Chemother.* 67(7), 1589-1596.

500 Long, Y., Ni, J., Wang, Z., 2015. Subcellular mechanism of *Escherichia coli* inactivation
501 during electrochemical disinfection with boron-doped diamond anode: A comparative
502 study of three electrolytes. *Water Res.* 84, 198–206.

503 Machado, L.F., Pereira, R.N., Martins, R.C., Teixeira, J.A., Vicente, A.A., 2010. Moderate
504 electric fields can inactivate *Escherichia coli* at room temperature. *J. Food Eng.* 96(4),
505 520–527.

506 Martínez-Huitle, C.A., 2007. Conductive diamond electrodes for water purification. *Mater.*
507 *Res.* 10(4), 419–424.

508 Martínez-Huitle, C.A., Brillas, E., 2008. Electrochemical alternatives for drinking water
509 disinfection. *Angew. Chem. Int. Ed.* 47(11), 1998–2005.

510 Martínez-Huitle, C.A., Rodrigo, M.A., Sirés, I., Scialdone, O., 2015. Single and coupled
511 electrochemical processes and reactors for the abatement of organic water pollutants: A
512 critical review. *Chem. Rev.* 115(24), 13362–13407.

513 Mascia, M., Vacca, A., Palmas, S., 2012. Fixed bed reactors with three dimensional
514 electrodes for electrochemical treatment of waters for disinfection. *Chem. Eng. J.* 211-
515 212, 479-487.

516 Mascia, M., Vacca, A., Palmas, S., 2013. Electrochemical treatment as a pre-oxidative step
517 for algae removal using *Chlorella vulgaris* as a model organism and BDD anodes.
518 *Chem. Eng. J.* 219, 512-519.

519 Nakajima, N., Nakano, T., Harada, F., Taniguchi, H., Yokoyama, I., Hirose, J., Daikoku, E.
520 Sano, K., 2004. Evaluation of disinfective potential of reactivated free chlorine in
521 pooled tap water by electrolysis. *J. Microbiol. Meth.* 57(2), 163–173.

522 Oturan, N., Brillas, E., Oturan, M.A., 2012. Unprecedented total mineralization of atrazine
523 and cyanuric acid by anodic oxidation and electro-Fenton with a boron-doped diamond
524 anode. *Environ. Chem. Lett.* 10 (2), 165-170.

525 Panizza, M., Cerisola, G., 2008. Electrochemical degradation of methyl red using BDD and
526 PbO_2 anodes. *Ind. Eng. Chem. Res.* 47(18), 6816–6820.

527 Panizza, M., Cerisola, G., 2009. Direct and mediated anodic oxidation of organic pollutants.

528 Chem. Rev. 109(12), 6541–69.

529 Pípi, A.R.F., De Andrade, A., Brillas, E., Sirés, I., 2014. Total removal of alachlor from water
530 by electrochemical processes. Sep. Purif. Technol. 132, 674-683.

531 Polcaro, A.M., Vacca, A., Mascia, M., Palmas, S., Pompei, R., Laconi, S., 2007.
532 Characterization of a stirred tank electrochemical cell for water disinfection processes.
533 Electrochim. Acta 52(7), 2595–2602.

534 Rajab, M., Heim, C., Letzel, T., Drewes, J.E., Helmreich, B., 2015. Electrochemical
535 disinfection using boron-doped diamond electrode –The synergetic effects of in situ
536 ozone and free chlorine generation. Chemosphere 121, 47-53.

537 Rodrigo, M.A., Cañizares, P., Sánchez-Carretero, A., Sáez, C., 2010. Use of conductive-
538 diamond electrochemical oxidation for wastewater treatment. Catal. Today 151(1-2),
539 173–177.

540 Scialdone, O., Corrado, E., Galia, A., Sirés, I., 2014. Electrochemical processes in macro and
541 microfluidic cells for the abatement of chloroacetic acid from water. Electrochim. Acta
542 132, 15-24.

543 Shang, K., Qiao, Z., Sun, B., Fan, X., Ai, S., 2013. An efficient electrochemical disinfection
544 of *E. coli* and *S. aureus* in drinking water using ferrocene–PAMAM–multiwalled
545 carbon nanotubes–chitosan nanocomposite modified pyrolytic graphite electrode. J.
546 Solid State Electrochem. 17(6), 1685–1691.

547 Sirés, I., Brillas, E., 2012. Remediation of water pollution caused by pharmaceutical residues
548 based on electrochemical separation and degradation technologies: A review. Environ.
549 Int. 40(1), 212–229.

550 Sirés, I., Brillas, E., Oturan, M.A., Rodrigo, M.A., Panizza, M., 2014. Electrochemical
551 advanced oxidation processes: Today and tomorrow. A review. Environ. Sci. Pollut.
552 Res. 21(14), 8336–8367.

553 Thiam, A., Brillas, E., Centellas, F., Cabot, P.L., Sirés, I., 2015a. Electrochemical reactivity
554 of Ponceau 4R (food additive E124) in different electrolytes and batch cells.
555 Electrochim. Acta 173, 523-533.

556 Thiam, A., Sirés, I., Garrido, J.A., Rodríguez, R.M., Brillas, E., 2015b. Effect of anions on
557 electrochemical degradation of azo dye Carmoisine (Acid Red 14) using a BDD anode
558 and air-diffusion cathode. Sep. Purif, Technol. 140, 43–52.

559 Thiam, A., Brillas, E., Garrido, J.A., Rodríguez, R.M., Sirés, I., 2015c. Routes for the
560 electrochemical degradation of the artificial food azo-colour Ponceau 4R by advanced
561 oxidation processes. Appl. Catal. B: Environ. 180, 227–236.

562 Vacca, A., Mascia, M., Palmas, S., Mais, L., Rizzardini, S., 2013. On the formation of
563 bromate and chlorate ions during electrolysis with boron doped diamond anode for
564 seawater treatment. J. Chem. Technol. Biotechnol. 88(12), 2244-2251.

565 Van Elsas, J.D, Dijkstra, A.F, Govaert, J.M., Van Veen, J.A., 1986. Survival of *Pseudomonas*
566 *fluorescens* and *Bacillus subtilis* introduced into two soils of different texture in field
567 microplots. FEMS Microbiol. Ecol. 2(3), 151-160.

568 Weaver, J.C., Chizmadzhev, Y.A., 1996. Theory of electroporation: A review.
569 Bioelectrochem. Bioenerg. 41(2), 135–160.

570 Werschkun, B., Sommer, Y., Banerji, S., 2012. Disinfection by-products in ballast water
571 treatment: An evaluation of regulatory data. Water Res. 46(16), 4884–4901.

572 World Health Organization (WHO), 2015. Drinking-water. Fact Sheet, n° 391. Available at:
573 <http://www.who.int/mediacentre/factsheets/fs391/en/> [Accessed April 6, 2016].

574 Yao, Y., Kubota, Y., Murakami, T., Ochiai, T., Ishiguro, H., Nakata, K., Fujishima, A., 2011.
575 Electrochemical inactivation kinetics of boron-doped diamond electrode on waterborne
576 pathogens. J. Water Health 9(3), 534–543.

577 Yoon, K.Y., Byeon, J.H., Park, J.H., Hwang, J., 2007. Susceptibility constants of *Escherichia*
578 *coli* and *Bacillus subtilis* to silver and copper nanoparticles. *Sci. Total Environ.* 373(2),
579 572-575.
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581 **Figure captions**

582 **Fig. 1.** Logarithmic reduction of bacterium content with electrolysis time for the
583 electrochemical oxidation (EO) treatment of 100 mL of aqueous suspensions with 7 mM
584 Na₂SO₄ and 10⁶ CFU mL⁻¹ of a given bacterium using a BDD/stainless steel cell at 33.3 mA
585 cm⁻² and 25 °C. Bacterium: *Escherichia coli* (EC), *Pseudomonas aeruginosa* (PA), *Bacillus*
586 *atrophaeus* (BA), *Staphylococcus aureus* (SA) and *Enterococcus hirae* (EH). The number 3
587 or 7 in each acronym accounts for the initial solution pH, i.e., 3.0 or 7.0, respectively.

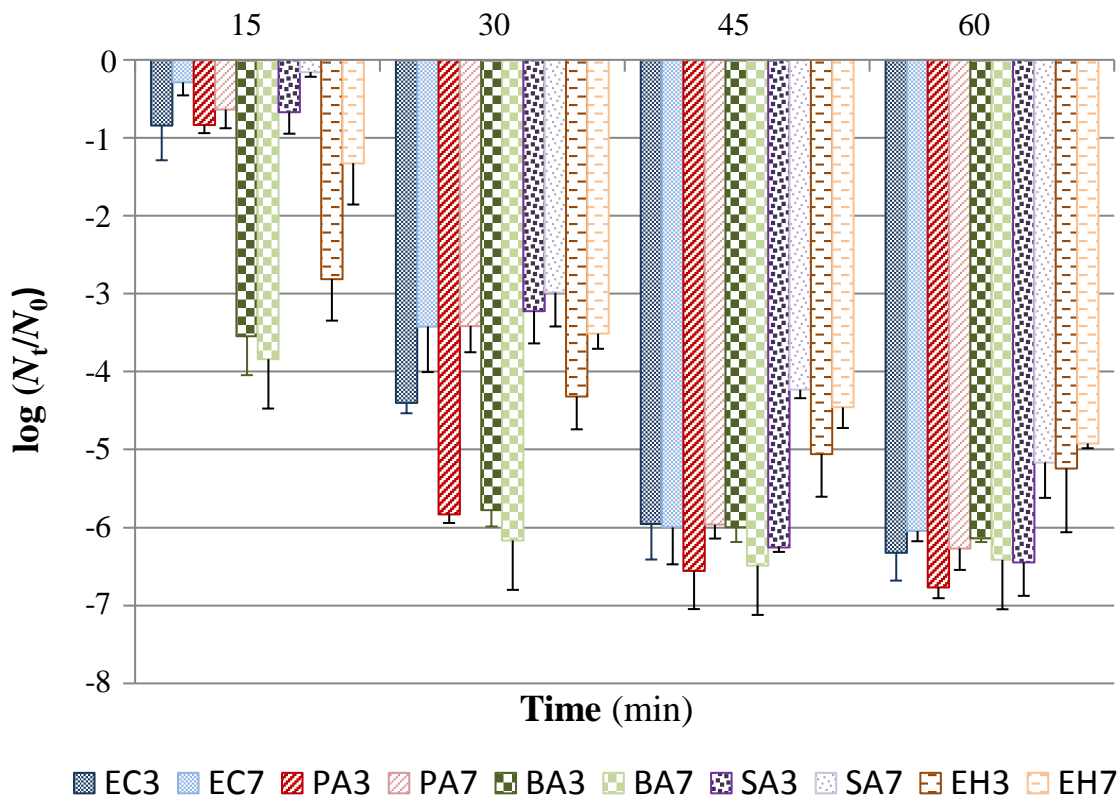
588 **Fig. 2.** Logistic model applied to the electrochemical inactivation kinetics of: (a) *E. coli* (b),
589 *P. aeruginosa*, (c) *B. atrophaeus*, (d) *S. aureus* and (e) *E. hirae* during the EO trials shown in
590 Fig. 1. The dashed lines represent the 95% confidence intervals on these fits.

591 **Fig. 3.** SEM images for: (a) *E. coli* (b), *P. aeruginosa*, (c) *B. atrophaeus*, (d) *S. aureus* and (e)
592 *E. hirae* supported on polycarbonate membrane filters. Samples correspond to bacteria
593 suspensions in 7 mM Na₂SO₄ at pH 7.0, before (left) and after (right) 45 min of EO treatment
594 with a BDD/stainless steel cell at 33.3 mA cm⁻² and 25 °C.

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Fig. 1

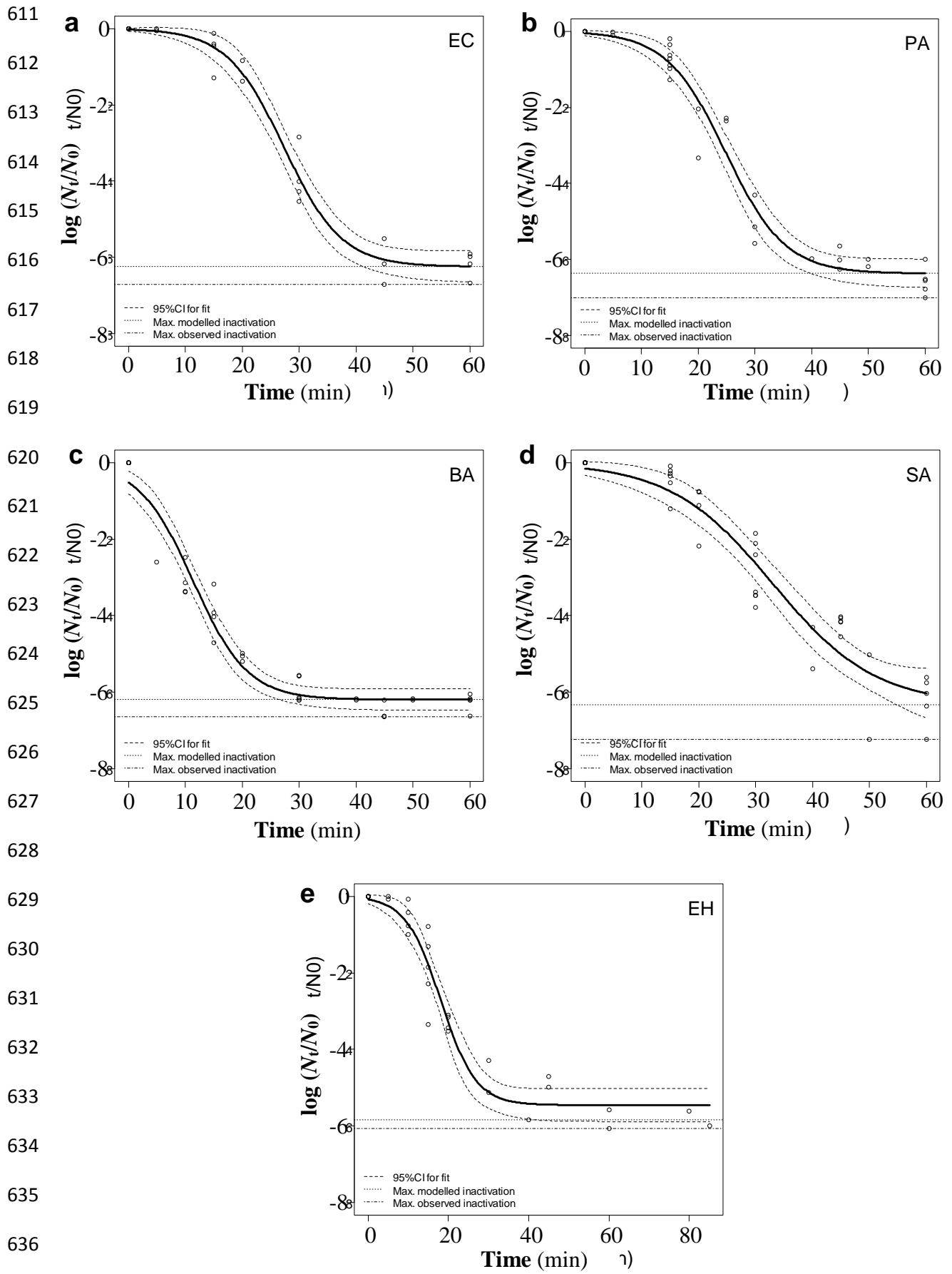
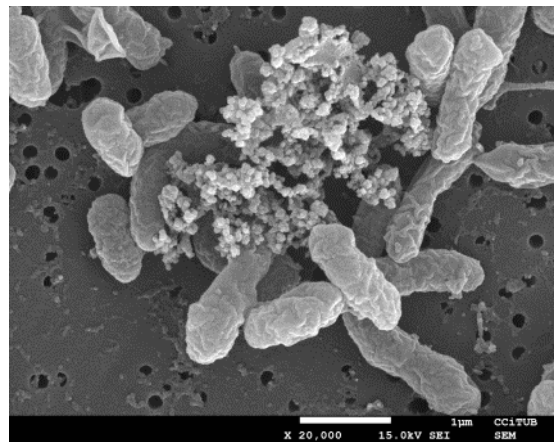
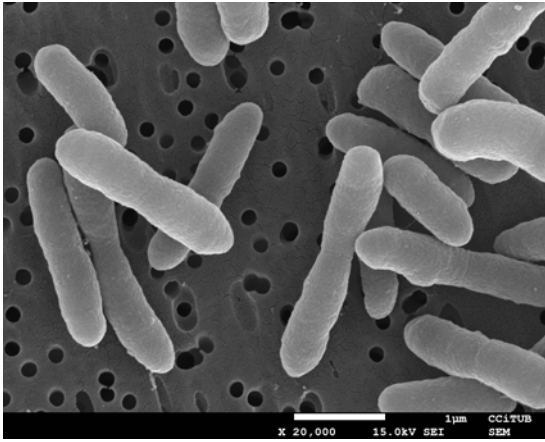


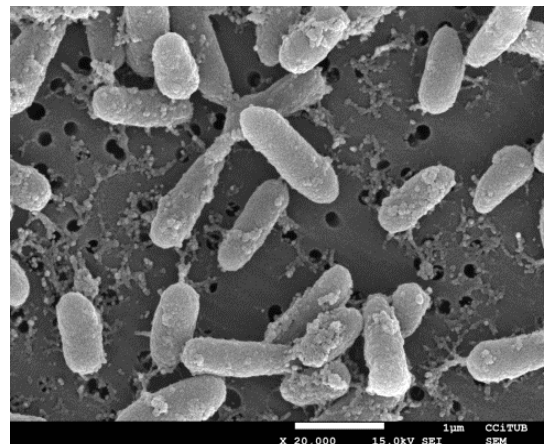
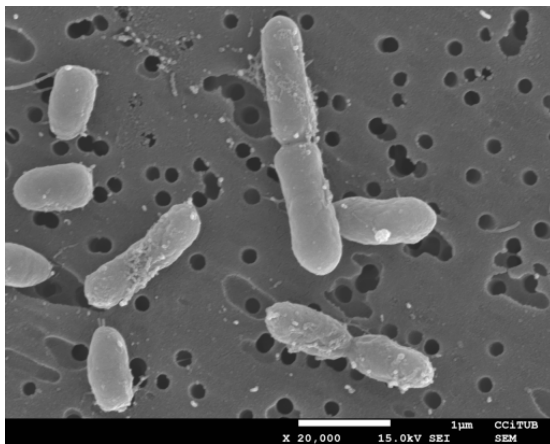
Fig. 2

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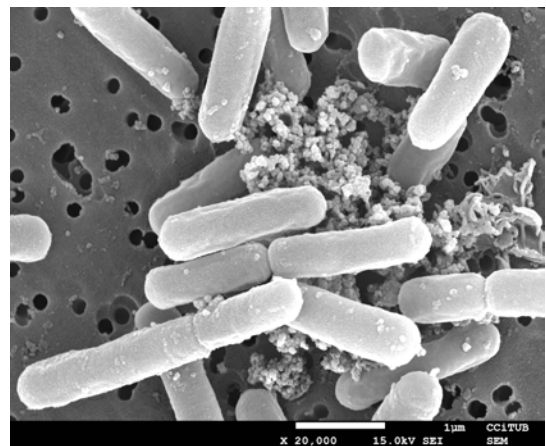
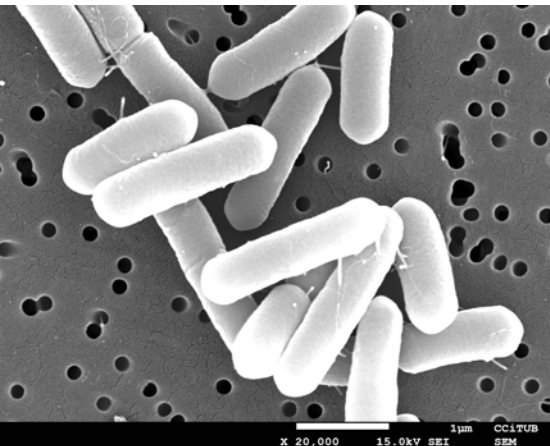
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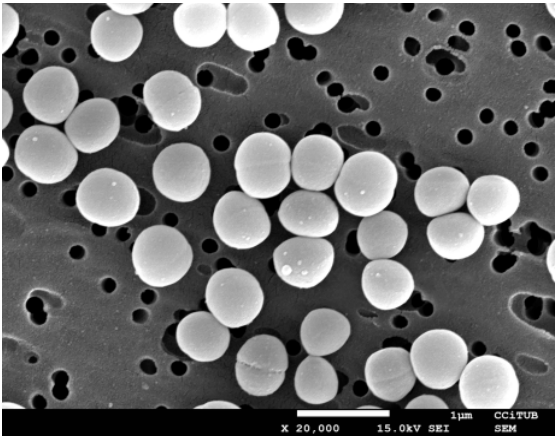
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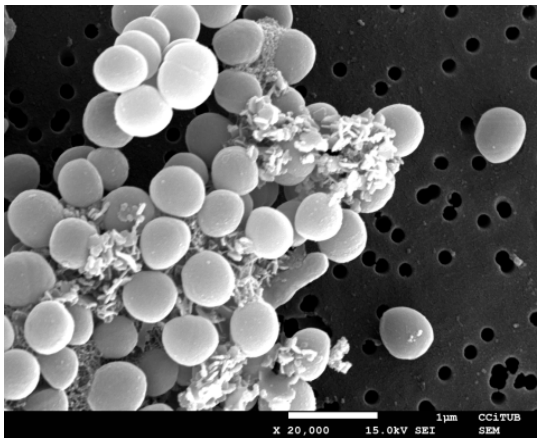
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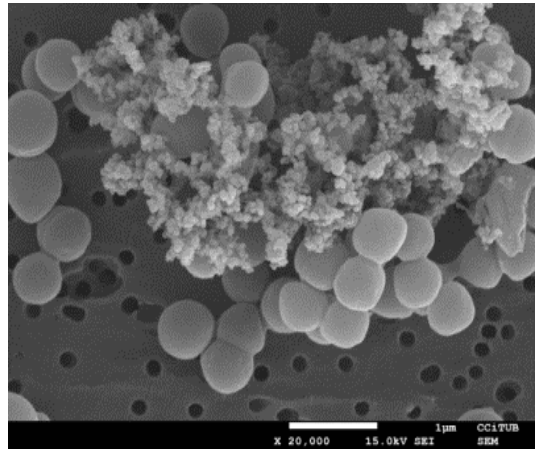
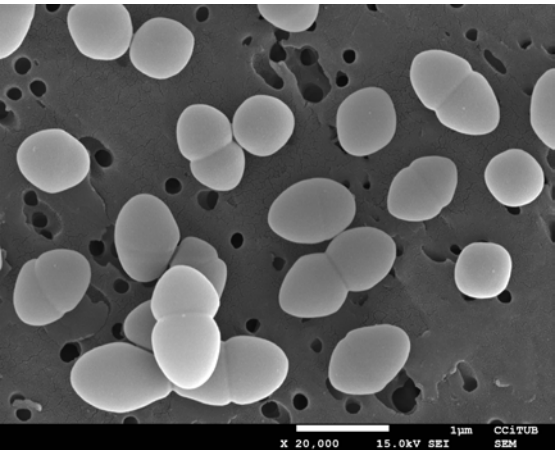


Fig. 3

693 Table 1

694 Parameters and goodness of fit for the logistic model curves of Fig. 2 for each bacterium.

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| Parameter | <i>E. coli</i> | <i>P. aeruginosa</i> | <i>B. atrophaeus</i> | <i>S. aureus</i> | <i>E. hirae</i> |
|-----------|----------------|----------------------|----------------------|------------------|-----------------|
| <i>I</i> | -6.243 | -6.369 | -6.192 | -6.327 | -5.453 |
| <i>a</i> | 228.958 | 115.509 | 10.810 | 39.166 | 63.981 |
| <i>i</i> | -0.198 | -0.192 | -0.2092 | -0.111 | -0.229 |
| R^2 | 0.979 | 0.971 | 0.964 | 0.942 | 0.955 |

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699 Table 2

700 Time required for selected inactivation ratios expressed in percentage for each bacterium
701 using the logistic model of Eq. (1).

702

| Bacterium | Time for inactivation ratios (min) | | | | |
|----------------------|------------------------------------|----------|------------|-------------|--------------|
| | T_{90} | T_{99} | $T_{99.9}$ | $T_{99.99}$ | $T_{99.999}$ |
| <i>E. coli</i> | 19.1 | 23.6 | 27.1 | 30.4 | 34.5 |
| <i>P. aeruginosa</i> | 15.9 | 20.7 | 24.1 | 27.5 | 31.5 |
| <i>B. atrophaeus</i> | 3.5 | 7.8 | 11.1 | 14.2 | 18.2 |
| <i>S. aureus</i> | 17.9 | 26.1 | 32.1 | 37.9 | 45.0 |
| <i>E. hirae</i> | 11.6 | 15.7 | 19.0 | 22.6 | 28.6 |

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