

# Double-diffusive Hadley-Prats flow in a horizontal porous layer with a concentration based internal heat source

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## Abstract

Double-diffusive Hadley-Prats flow with a concentration based heat source is investigated through linear and non-linear stability analyses. The resultant eigenvalue problems for both theories are solved numerically using Shooting and fourth order Runge-Kutta methods, with the critical thermal Rayleigh number being evaluated with respect to various flow governing parameters such as the magnitudes of the heat source and mass flow. It is observed, in the linear case, that an increase in the horizontal thermal Rayleigh number is stabilising for both positive and negative values of the solutal Rayleigh number. In non-linear case, a destabilizing effect is identified at higher mass flow rates. An increase in both the heat source and mass flow results in destabilisation.

*Key words:* Double diffusive convection, porous medium, heat source, mass flow, Energy stability analysis.

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## 1 Introduction

Double-diffusive convection in a fluid-saturated porous media has received much attention during the last few decades, due to its many real-world applications such as underground energy transport (Nagano et al. [1]), food processing, oil recovery, the spreading of pollutants etc. (Bendrichi and Shemilt [2]; Reddy et al. [3]) and multiple

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environmental processes (Xi and Li[4] and Kwon et al. [5]). A collection of comprehensive theories and experiments on double diffusive convection in porous media are presented in Ingham and Pop [6], Vafai [7], Nield and Bejan [8].

Of particular interest to the present study are investigations focusing on the phenomenon of double-diffusive convection in a shallow horizontal layer of a porous medium subject to inclined thermal and solutal gradients at both walls. Concerning the mono-diffusive case, non-homogeneity on the temperature conditions at both walls induces a basic flow (Hadley flow), which was first studied by Weber [13], and extended by Nield [14]. Nield et al. [15] further studied double diffusive Hadley flow due to inclined thermal and solutal gradients in a fluid saturated horizontal porous medium. An extension of this work with horizontal mass flow is due to Manole et al. [16]. If the flow is subjected to horizontal mass flow along with inclined thermal gradients, the resultant flow is known as Hadley-Prats flow (Barletta and Nield [17]). All the aforementioned works are related to linear stability analysis, to determine the critical values of the problem parameters and the nature of the instability in a well packed, low permeability porous media, so that the flow in the porous medium can be represented by Darcy flow model.

In the Lyapunov sense, linear stability theory gives sufficient conditions for instability, where the disturbance of the basic flow is unstable, whereas non-linear theory provides a sufficient condition for the disturbance to be asymptotically stable. Several problems in non-linear stability analysis using energy method are discussed by Kaloni and his contributors (Guo and Kaloni [9]; Kaloni and Qiao [10]; Kaloni and Qiao [11]). A collection of available studies for non-linear theory is given by Straughan [12]. The development of both linear instability and energy stability theories allows for the assessment of potential regions of subcritical instabilities in which convection could commence before the linear instability threshold is reached.

The motivation of the present work is to investigate double-diffusive Hadley flow in porous media induced by the active absorption of radiation, as demonstrated by

Krishnamurti [18] for a viscous fluid in the absence of Hadely circulation and Hill [19] for flows through porous media. Their model has received much attention in recent years as it provides an accurate model of cumulus convection as it occurs in the atmosphere. In addition to exploring a linear theory for the double-diffusive Hadley-Prats flow with concentration based internal heat source, we develop a complementary energy theory. The use of energy theory in the context of double-diffusive convection has been utilised extensively including Carr [20], Guo and Kaloni [9] and Hill [19]. We organize the paper in the following manner: section 2 constructs the governing equations of the model under consideration; in sections 3 & 4 we discuss the basic-state solution and perturbation equations; in sections 5 & 6 linear and non-linear analyses are performed, respectively, with the results and conclusions being discussed in sections 7 and 8, respectively.

## 2 Governing Equations

An infinite shallow horizontal fluid saturated porous layer with height  $d$ , confined between two isothermal and isosolutal fixed plates with concentration based internal heat source  $Q^*$  is considered. The Cartesian coordinates are chosen such that the  $z^*$ -axis is vertically upwards and there is a net flow along the direction of  $x^*$ -axis with magnitude  $u_0$  as given in Fig. 1. A uniform concentration difference  $\nabla S$  and a temperature difference  $\nabla \theta$  are maintained between the lower and upper plates. Flow in the porous medium is governed by the Darcy law and the Oberbeck-Boussinesq approximation is invoked (such that the density variations are assumed to be sufficiently small to be neglected everywhere except in the body force term), and density  $\rho_f^*$  of the fluid is given by

$$\rho_f^* = \rho_0 [1 - \gamma_S (S^* - S_0) - \gamma_\theta (\theta^* - \theta_0)],$$

where  $S^*$  is the concentration,  $\theta^*$  is the temperature,  $\gamma_S$  and  $\gamma_\theta$  are the volumetric solutal and thermal expansion coefficients in the porous medium, and  $\rho_0$  is the density at concentration  $S_0$  and temperature  $\theta_0$ . The governing system is given by the Darcy

velocity in porous media, the concentration equation and the temperature equation such that

$$\nabla^* \cdot \mathbf{q}^* = 0, \quad (1)$$

$$\frac{\mu}{K} \mathbf{q}^* + \nabla^* P^* - \rho_f^* g_0 \mathbf{k} = 0, \quad (2)$$

$$\phi \left( \frac{\partial S^*}{\partial t^*} \right) + \mathbf{q}^* \cdot \nabla^* S^* = D_m \nabla^{*2} S^* \quad (3)$$

$$(\rho c)_m \left( \frac{\partial \theta^*}{\partial t^*} \right) + (\rho c_p)_f \mathbf{q}^* \cdot \nabla^* \theta^* = k_m \nabla^{*2} \theta^* + Q^* (S^* - S_0), \quad (4)$$

where Eq. (1) is the incompressibility condition. The boundary conditions are given by

$$z^* = -\frac{1}{2}d: \quad w^* = 0, \quad S^* = S_0 + \frac{\Delta S}{2} - \beta_{S_x} x^* - \beta_{S_y} y^*, \quad \theta^* = \theta_0 + \frac{\Delta \theta}{2} - \beta_{\theta_x} x^* - \beta_{\theta_y} y^*,$$

$$z^* = \frac{1}{2}d: \quad w^* = 0, \quad S^* = S_0 - \frac{\Delta S}{2} - \beta_{S_x} x^* - \beta_{S_y} y^*, \quad \theta^* = \theta_0 - \frac{\Delta \theta}{2} - \beta_{\theta_x} x^* - \beta_{\theta_y} y^*. \quad (5)$$

Here  $\mathbf{q}^* = (u^*, v^*, w^*)$  is the velocity,  $P^*$  is the pressure,  $\mu$  is the viscosity,  $D_m$  is the solutal diffusivity,  $k_m$  is the thermal conductivity,  $g_0$  is the gravity acceleration and  $\mathbf{k}$  is the unit vector in the  $z^*$ -direction. The imposed horizontal components of solutal and thermal gradients to be  $(\beta_{S_x}, \beta_{S_y})$  and  $(\beta_{\theta_x}, \beta_{\theta_y})$ , respectively.  $K$  and  $\phi$  are the permeability and porosity of the medium, respectively. The subscripts  $f$  and  $m$  refer to the fluid and porous medium, respectively.  $c_p$  and  $c$  are the specific heats of the fluid and solid components. Here  $(\rho c_p)_f$  and  $(\rho c)_m$  are volumetric heat capacities for the fluid and solid phases. Following the scaling of Weber [13] and Nield [14], we define

$$x = \frac{x^*}{d}, \quad y = \frac{y^*}{d}, \quad z = \frac{z^*}{d}, \quad t = \frac{\alpha_m t^*}{ad^2}, \quad q = \frac{dq^*}{\alpha_m}, \quad P = \frac{K(P^* + \rho_0 g_0 z^*)}{\mu \alpha_m},$$

$$\theta = \frac{R_z(\theta^* - \theta_0)}{\Delta \theta}, \quad S = \frac{S_z(S^* - S_0)}{\Delta S}, \quad Q = \frac{Q^* d^2 R_z \Delta S}{k_m S_z \Delta \theta} \quad (6)$$

where

$$\alpha_m = \frac{k_m}{(\rho c_p)_f}, \quad a = \frac{(\rho c)_m}{(\rho c_p)_f}, \quad S_z = \frac{\rho_0 g_0 \gamma_S K d \Delta S}{\mu D_m}, \quad R_z = \frac{\rho_0 g_0 \gamma_\theta K d \Delta \theta}{\mu \alpha_m}. \quad (7)$$

Here,  $S_z$  and  $R_z$  denote the vertical solutal and thermal Rayleigh numbers, respectively.

The horizontal solutal and thermal Rayleigh numbers are defined as follows

$$\begin{aligned} S_x &= \frac{\rho_0 g_0 \gamma_S K d^2 \beta_{S_x}}{\mu D_m}, & S_y &= \frac{\rho_0 g_0 \gamma_S K d^2 \beta_{S_y}}{\mu D_m}, \\ R_x &= \frac{\rho_0 g_0 \gamma_\theta K d^2 \beta_{\theta_x}}{\mu \alpha_m}, & R_y &= \frac{\rho_0 g_0 \gamma_\theta K d^2 \beta_{\theta_y}}{\mu \alpha_m}, \end{aligned} \quad (8)$$

with  $Le = \frac{\alpha_m}{D_m}$  being Lewis number and the non-dimensional net flow along the horizontal direction is defined as the Peclet number  $M = \frac{u_0 d}{\alpha_m}$ . Under these dimensionless variables, the governing Eqs. (1) - (4) take the following non-dimensional form

$$\nabla \cdot \mathbf{q} = 0, \quad (9)$$

$$\mathbf{q} + \nabla P - \left( \frac{1}{Le} S + \theta \right) \mathbf{k} = 0, \quad (10)$$

$$\left( \frac{\phi}{a} \right) \frac{\partial S}{\partial t} + \mathbf{q} \cdot \nabla S = \frac{1}{Le} \nabla^2 S, \quad (11)$$

$$\frac{\partial \theta}{\partial t} + \mathbf{q} \cdot \nabla \theta = \nabla^2 \theta + QS, \quad (12)$$

with boundary conditions

$$\begin{aligned} z = -\frac{1}{2} : & \quad w = 0, \quad S = \frac{S_z}{2} - S_x x - S_y y, \quad \theta = \frac{R_z}{2} - R_x x - R_y y, \\ z = \frac{1}{2} : & \quad w = 0, \quad S = -\frac{S_z}{2} - S_x x - S_y y, \quad \theta = -\frac{R_z}{2} - R_x x - R_y y. \end{aligned} \quad (13)$$

From Eqs. (9) - (12) we observe that all of the solutal and thermal Rayleigh numbers appear in the boundary conditions (13).

### 3 Steady-State Solution

Governing equations (9)-(12), subject to boundary conditions (13) admit a basic state solution of the form

$$\begin{aligned} S_s &= \tilde{S}(z) - S_x x - S_y y, & \theta_s &= \tilde{\theta}(z) - R_x x - R_y y, \\ u_s &= u(z), & v_s &= v(z), & w_s &= 0, & P_s &= P(x, y, z), \end{aligned} \quad (14)$$

where

$$\begin{aligned}
u &= -\frac{\partial P}{\partial x}, \quad v = -\frac{\partial P}{\partial y}, \\
0 &= -\frac{\partial P}{\partial z} + \left[ \frac{1}{Le} \left( \tilde{S}(z) - S_x x - S_y y \right) + \tilde{\theta}(z) - R_x x - R_y y \right], \\
\frac{1}{Le} D^2 \tilde{S} &= -u S_x - v S_y, \quad D^2 \tilde{\theta} + QS = -u R_x - v R_y.
\end{aligned} \tag{15}$$

Here  $D = \frac{d}{dz}$  and  $M = \int_{-1/2}^{1/2} u(z) dz$  is the net flow in the horizontal direction and  $\int_{-1/2}^{1/2} v(z) dz = 0$ . Peclet number  $M$  gives the strength of flow along the horizontal direction. We obtain the basic state solution in the form of flow velocity, concentration and temperature in the medium such that

$$u_s = \left( \frac{S_x}{Le} + R_x \right) z + M, \quad v_s = \left( \frac{S_y}{Le} + R_y \right) z, \quad w_s = 0, \tag{16}$$

$$\tilde{S} = -S_z z + A, \quad \tilde{\theta} = -R_z z + B, \tag{17}$$

where  $A$ ,  $B$ ,  $\lambda_1$  and  $\lambda_2$  are given by

$$\begin{aligned}
A &= \frac{\lambda_1}{24} (z - 4z^3) + \frac{MS_x Le}{8} (1 - 4z^2), \\
B &= \frac{(\lambda_2 - QS_z)}{24} (z - 4z^3) - \frac{MR_x}{8} (4z^2 - 1) + \frac{\lambda_1 Q}{24} (z^5/5 - z^3/6 + 7z/240) \\
&\quad - \frac{QMLeS_x}{8} (z^2/2 - z^4/3) + \frac{5MS_x LeQ}{384}, \\
\lambda_1 &= S_x^2 + S_y^2 + Le(R_x S_x + R_y S_y), \quad \lambda_2 = R_x^2 + R_y^2 + \frac{R_x S_x + R_y S_y}{Le}.
\end{aligned} \tag{18}$$

The flow given by Eq. (16) is referred to as the Hadley-Prats flow.

#### 4 Perturbation Equations

Introducing a perturbation of the form  $q = q_s + q'$ ,  $S = S_s + S'$ ,  $\theta = \theta_s + \theta'$  and  $P = P_s + P'$ , and substituting these perturbations into the dimensionless governing equations (9) - (12) yields

$$\nabla \cdot q' = 0, \tag{19}$$

$$q' = -\nabla P' + \left( \frac{S'}{Le} + \theta' \right) \mathbf{k}, \tag{20}$$

$$\left(\frac{\phi}{a}\right) \frac{\partial S'}{\partial t} + q_s \cdot \nabla S' + q' \cdot \nabla S_s + q' \cdot \nabla S' = \frac{1}{Le} \nabla^2 S', \quad (21)$$

$$\frac{\partial \theta'}{\partial t} + q_s \cdot \nabla \theta' + q' \cdot \nabla \theta_s + q' \cdot \nabla \theta' = \nabla^2 \theta' + QS', \quad (22)$$

where

$$\nabla S_s = -\left(S_x, S_y, S_z - \tilde{A}\right), \quad \nabla \theta_s = -\left(R_x, R_y, R_z - \tilde{B}\right),$$

$$\tilde{A} = \frac{\lambda_1}{24} [1 - 12z^2] - MS_x Lez,$$

$$\tilde{B} = \frac{(\lambda_2 - QS_z)}{24} (1 - 12z^2) + \frac{\lambda_1 Q}{24} \left(z^4 - \frac{z^2}{2} + \frac{7}{240}\right) - \frac{QMLeS_x}{24} (3z - 4z^3) - MR_x z.$$

The boundary conditions are

$$w' = 0, \quad S' = 0, \quad \theta' = 0, \quad \text{at } z = \pm \frac{1}{2}, \quad (23)$$

which state that there is zero perturbation in velocity, concentration and temperature at the upper and lower plates.

## 5 Linear Stability Analysis

The linearized perturbation equations are derived by neglecting the products of disturbances from Eqs. (19) - (22), yielding

$$\nabla \cdot q' = 0, \quad (24)$$

$$q' = -\nabla P' + \left(\frac{S'}{Le} + \theta'\right) \mathbf{k}, \quad (25)$$

$$\left(\frac{\phi}{a}\right) \frac{\partial S'}{\partial t} + u_s \frac{\partial S'}{\partial x} + v_s \frac{\partial S'}{\partial y} - S_x u' - S_y v' + (D\tilde{S}) w' = \frac{1}{Le} \nabla^2 S', \quad (26)$$

$$\frac{\partial \theta'}{\partial t} + u_s \frac{\partial \theta'}{\partial x} + v_s \frac{\partial \theta'}{\partial y} - R_x u' - R_y v' + (D\tilde{\theta}) w' = \nabla^2 \theta' + QS', \quad (27)$$

where

$$D\tilde{S} = -S_z + \frac{\lambda_1}{24} [1 - 12z^2] - MS_x Lez,$$

$$D\tilde{\theta} = -R_z + \frac{(\lambda_2 - QS_z)}{24} (1 - 12z^2) + \frac{\lambda_1 Q}{24} \left(z^4 - \frac{z^2}{2} + \frac{7}{240}\right) - \frac{QMLeS_x}{24} (3z - 4z^3) - MR_x z. \quad (28)$$

Since the resulting system is linear and autonomous, we may seek solutions of the normal modes form

$$[q', S', \theta', P'] = [q(z), S(z), \theta(z), P(z)] \exp \{i(kx + ly - \sigma t)\} \quad (29)$$

and eliminate  $P$  from Eq. (25), to give

$$(D^2 - \alpha^2) w + \left(\frac{S}{Le} + \theta\right) \alpha^2 = 0, \quad (30)$$

$$\left(\frac{1}{Le} [D^2 - \alpha^2] + i\frac{\phi}{a}\sigma - iku_s - ilv_s\right) S + i\frac{1}{\alpha^2} (kS_x + lS_y) Dw - (D\tilde{S}) w = 0, \quad (31)$$

$$(D^2 - \alpha^2 + i\sigma - iku_s - ilv_s) \theta + \frac{i}{\alpha^2} (kR_x + lR_y) Dw - (D\tilde{\theta}) w + QS = 0, \quad (32)$$

where  $i = \sqrt{-1}$  and  $\alpha = \sqrt{k^2 + l^2}$  is the overall wave number. Equations (30) - (32) are subject to  $w = S = \theta = 0$  at both the plates  $z = \pm\frac{1}{2}$  and constitute an eigenvalue problem for vertical thermal Rayleigh number  $R_z$  with  $\alpha, \phi, Le, S_x, S_y, S_z, R_x, R_y, \sigma, k$  and  $l$  as parameters. The critical value of  $R_z$  is located by minimising over  $\alpha$ . The term longitudinal disturbances are characterized by  $k = 0$ . Similarly, transverse disturbances are characterized by  $l = 0$ . Critical thermal Rayleigh number for the linear theory is given as  $R_z = \min_{\alpha} R_z$ . Numerical results for the linear theory are presented in section 7.

## 6 Non-Linear Stability Analysis

To obtain global non-linear stability bounds we multiply equations (20), (21) and (22) by  $q', \beta'$  and  $\theta'$ , respectively, and integrate over the periodicity cell, denoted by  $\Omega$ , which yields

$$\|q'\|^2 = \langle \theta' w' \rangle + \langle \beta' w' \rangle, \quad (33)$$

$$\frac{Le\phi}{2a} \frac{d\|\beta'\|^2}{dt} = -\langle (q' \cdot \nabla S_s) \beta' \rangle - \|\nabla \beta'\|^2, \quad (34)$$

$$\frac{1}{2} \frac{d\|\theta'\|^2}{dt} = -\langle (q' \cdot \nabla \theta_s) \theta' \rangle - \|\nabla \theta'\|^2 + QLe \langle \beta' \theta' \rangle, \quad (35)$$



where  $\beta' = \frac{S'}{L_e}$ , and  $\langle \cdot \rangle$  denotes the integration over  $\Omega$  and  $\|\cdot\|$  represents  $L^2(\Omega)$  norm.

We obtain the following energy functional from Straughan [12]

$$E(t) = \frac{\xi}{2} \|\theta'\|^2 + \frac{\eta L_e \phi}{2a} \|\beta'\|^2 \quad (36)$$

where  $\xi > 0$  and  $\eta > 0$  are coupling parameters. Eqs. (33) - (35) and Eq. (36) can be put in the form

$$\frac{dE}{dt} = \mathcal{I} - \mathcal{D}, \quad (37)$$

where

$$\mathcal{I} = -\xi \langle (q' \cdot \nabla \theta_s) \theta' \rangle - \eta \langle (q' \cdot \nabla S_s) \beta' \rangle + \langle \theta' w' \rangle + \langle \beta' w' \rangle + \xi L_e Q \langle \beta' \theta' \rangle, \quad (38)$$

$$\mathcal{D} = \eta \|\nabla \beta'\|^2 + \xi \|\nabla \theta'\|^2 + \|q'\|^2. \quad (39)$$

Defining

$$R_E = \max_{\mathcal{H}} \left( \frac{\mathcal{I}}{\mathcal{D}} \right) \quad (40)$$

where  $\mathcal{H}$  is the space of all admissible solutions to equations (19) - (22), we have

$$\frac{dE}{dt} \leq -\mathcal{D} (1 - R_E). \quad (41)$$

The classical Poincaré inequality  $\|q' - q'_\Omega\|_{L^p(\Omega)} \leq C \|\nabla q'\|_{L^p(\Omega)}$ , where  $\Omega$  is a open connected locally compact Hausdorff space and use of  $q'_\Omega = \frac{1}{|\Omega|} \int_\Omega q'(y) dy$  yields

$$\frac{dE}{dt} \leq -2\pi^2 (1 - R_E) \min\left\{1, \frac{a}{L_e \phi}\right\} E. \quad (42)$$

The inequality (42) guarantees that  $E(t) \rightarrow 0$  at least exponentially as  $t \rightarrow \infty$  for  $R_E < 1$ . Since  $E(t)$  does not contain the kinetic energy term for the velocity  $\|q'\|^2$ , we apply the arithmetic-geometric mean inequality to Eq. (33) to yield

$$\|q'\|^2 \leq 2 \left( \|\beta'\|^2 + \|\theta'\|^2 \right). \quad (43)$$

From Eqs. (43) and (36) observed that the decay of  $\|q'\|$  is implied by the decay of  $E(t)$  and hence the system is stable for  $R_E < 1$ . The corresponding Euler-Lagrange system

for  $R_E$  is

$$\xi\theta'\nabla\theta_s + \eta\beta'\nabla S_s - (\theta' + \beta')\mathbf{k} + 2R_E q' = \nabla\pi', \quad (44)$$

$$w' - \eta q' \cdot \nabla S_s + LeQ\xi\theta' + 2R_E\eta\nabla^2\beta' = 0, \quad (45)$$

$$w' - \xi q' \cdot \nabla\theta_s + Q\xi\beta'z + 2R_E\xi\nabla^2\theta' = 0. \quad (46)$$

Here  $\pi'$  is Lagrange multiplier introduced because  $q'$  is divergence free. While deriving the Eqs. (44) - (46), we let  $\chi = (q', \beta', \theta')$  and  $L = \mathcal{I} - R_E\mathcal{D}$ . Then the corresponding Euler-Lagrange system can be written as

$$\nabla_{x_i}L - \frac{\partial}{\partial x_j}\nabla_{x_i\circ}L = 0 \quad \text{for } i = 1, 2, 3; \quad j = 1, 2, 3$$

where ' $\circ$ ' denotes the differentiation with respect to  $z$ . We consider  $R_z$  as the eigenvalue and estimate the maximum variation of  $R_z$  with optimal choice of  $\eta$  and  $\xi$ . From Eqs. (44) - (46) we can derive

$$\frac{\partial R_z}{\partial \eta} = \frac{2(1 + \xi R_z) [R_E(1 - \eta S_z) \|\nabla\beta'\|^2 + LeQ\xi S_z \langle \theta' \beta' \rangle + \langle \tilde{A}\beta' w' \rangle - \Psi_S]}{\xi^2(1 + \eta S_z) (2R_E \|\nabla\theta'\|^2 + \langle \tilde{B}\theta' w' \rangle - LeQ \langle \theta' \beta' \rangle - \Psi_R)}, \quad (47)$$

$$\frac{\partial R_z}{\partial \xi} = \frac{R_E(1 - \xi R_z) \|\nabla\theta'\|^2 + LeQ\xi R_z \langle \theta' \beta' \rangle + \langle \tilde{B}\theta' w' \rangle - \Psi_R}{\xi^2 (2R_E \|\nabla\theta'\|^2 + \langle \tilde{B}\theta' w' \rangle - LeQ \langle \theta' \beta' z \rangle - \Psi_R)}, \quad (48)$$

where

$$\Psi_S = S_x \langle \beta' u' \rangle + S_y \langle \beta' v' \rangle, \quad \Psi_R = R_x \langle \theta' u' \rangle + R_y \langle \theta' v' \rangle.$$

We also note that if  $S_x = S_y = 0$ ,  $R_x = R_y = 0$  and  $Q = 0$ , then

$$\frac{\partial R_z}{\partial \eta} = \frac{(1 + \xi R_z)(1 - \eta S_z) \|\nabla\beta'\|^2}{\xi^2(1 + \eta S_z) \|\nabla\theta'\|^2}, \quad (49)$$

$$\frac{\partial R_z}{\partial \xi} = \frac{(1 - \xi R_z)}{2\xi^2}, \quad (50)$$

which are also reported in Guo and Kaloni [9].

Equations (44) - (46) are solved for the critical value  $R_E = 1$ . To evaluate this system numerically, we take the *curl curl* of Eq. (44) and further use the third component

of the resulting equation, to find that

$$\begin{aligned} & \xi R_x \frac{\partial^2 \theta'}{\partial x \partial z} + \xi R_y \frac{\partial^2 \theta'}{\partial y \partial z} + \xi \nabla_1^2 [(-R_z + \tilde{B}) \theta'] + \eta S_x \frac{\partial^2 \beta'}{\partial x \partial z} + \eta S_y \frac{\partial^2 \beta'}{\partial y \partial z} + 2 \nabla_1^2 w' \\ & + \eta \nabla_1^2 [(-S_z + \tilde{A}) \beta'] - \nabla_1^2 (\theta' + \beta') - 2 \left( \frac{\partial^2 u'}{\partial x \partial z} + \frac{\partial^2 v'}{\partial y \partial z} \right) = 0, \end{aligned} \quad (51)$$

where  $\nabla_1^2 = \left( \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} \right)$ . Applying normal modes

$$[q', \beta', \theta', \pi'] = [q(z), \beta(z), \theta(z), \pi(z)] \exp(i(kx + ly)), \quad (52)$$

with  $(S_x, S_y) \cdot (k, l) = 0$ ;  $(R_x, R_y) \cdot (k, l) = 0$ , in Eqs. (44), (45), (46), (51) and eliminate  $u, v$  and  $\pi$  to obtain the following eigenvalue problem

$$D^2 w = \alpha^2 w + \alpha^2 \eta h_1 \beta + \alpha^2 \xi h_2 \theta, \quad (53)$$

$$D^2 \beta = -h_1 w + h_3 \beta - \xi h_4 \theta, \quad (54)$$

$$D^2 \theta = h_2 w - \eta h_4 \beta + h_5 \theta, \quad (55)$$

where

$$h_1 = \frac{1}{2} [-S_z + \tilde{A} - \eta^{-1}], \quad h_2 = \frac{1}{2} [-R_z + \tilde{B} - \xi^{-1}], \quad h_3 = \alpha^2 - \frac{\eta}{4} [S_x^2 + S_y^2],$$

$$h_4 = \frac{1}{4} [R_x S_x + R_y S_y + 2LeQ\eta^{-1}], \quad h_5 = \alpha^2 - \frac{\xi}{4} [R_x^2 + R_y^2],$$

and the corresponding boundary conditions are

$$w = \beta = \theta = 0 \quad \text{at} \quad z = \pm \frac{1}{2}. \quad (56)$$

The critical vertical thermal Rayleigh number is obtained through

$$R_z = \max_{\xi} \max_{\eta} \min_{\alpha} R_z(\xi, \eta, \alpha, Q, M, Le, R_x, R_y, S_x, S_y, S_z). \quad (57)$$

Numerical comparison between the linear and non-linear theories are presented in the next section.

## 7 Results and Discussion

Our goal in this study is to bring out the effect of a concentration based heat source on the double-diffusive Hadley-Prats flow in porous media. We apply the numerical scheme which is proposed by Barletta and Nield [21] to solve the eigenvalue problem (30) - (32) for linear and (53) - (55) for non-linear cases, with respect to the boundary conditions (56), in which, we treat vertical thermal Rayleigh number ( $R_z$ ) as the eigenvalue. Here, the critical  $R_z$  is defined as the minimum of all  $R_z$  values as  $\alpha$  is varied in both linear and non-linear cases. In our computations, we consider both cases  $S_z < 0$  and  $S_z > 0$ , where  $S_z > 0$  represents the concentration on upper boundary being higher than that of lower boundary, with  $S_z < 0$  being the reverse. In the present study, we set  $\phi/a = 1$ ,  $S_y = R_y = 0$  and  $Le = 10$  as this is roughly representative of experiments with sugar or salt systems. Barletta and Nield [21] concluded for the Hadley-Prats flow, that the preferred mode of the disturbance is the non-oscillatory longitudinal mode. Hence, the results presented here are for  $k = 0$  and  $\sigma = 0$ . In Table 1, the computation results of the critical values of  $R_z$  are illustrated for various values of  $S_z$  in the absence of horizontal Rayleigh numbers. In this table,  $R_{z_l}$  indicates critical  $R_z$  in linear case and  $R_{z_e}$  indicates the non-linear critical  $R_z$ . And also,  $\alpha_l$  indicates the critical wave number in linear case and  $\alpha_e$  indicates the critical wave number in non-linear case. From the Table 1, it is observed that when  $R_x = R_y = S_x = S_y = 0$ ,  $Q = 0$  and  $M = 0$  the present results are in very good agreement with the existing results in the literature, due to Guo and Kaloni [9]. For an increase in the value of  $S_z$  from negative to positive, the critical value of  $R_z$  is reduced in the both linear and non-linear cases seen in Table 1. This indicates that the system becomes unstable as  $S_z$  increases.

In Figs. 2 to 7, we used fixed notation to represent linear and non-linear results. In these figures solid lines represent the linear stability results and the dashed lines represent the non-linear stability results.

The response of critical values of  $R_z$  as a function of horizontal mass flow  $M$  for

both positive and negative values of  $S_z$  is shown in Figs. 2 and 3, respectively. In the absence of a heat source ( $Q$ ), the linear results shows that increasing the mass flow in the medium destabilizes the convection. When  $Q$  is introduced, and for smaller values of  $M$ , the flow is initially stabilized, but once the magnitude of  $M$  takes higher values, this causes the destabilization of the flow seen in Figs. 2 and 3. Increasing the value of  $Q$  reduces the critical values of  $R_z$  with increasing mass flow in the linear case for  $S_z > 0$  and  $S_z < 0$ . However, in the case of non-linear analysis, in the absence of  $Q$ , critical values of  $R_z$  are reduced with increasing the values of  $M$ , which is in contrast to the stabilization phenomenon observed in the linear case. From Fig. 3, when  $S_z = -3$  and  $M$  increases, then the critical values of  $R_z$  decreases irrespective of heat source ( $Q$ ) for both linear and non-linear cases. It means that the flow is destabilises as mass flow increases when  $S_z = -3$ . It is clearly observed that, when  $Q = 0$  (i.e. there is no concentration based internal heat source) the difference between the linear and non-linear critical values increases with an increase in  $M$ , whereas, in the presence of a heat source ( $Q > 0$ ), it is observed that this difference is reduced in Figs. 2 and 3. This indicates that, as the heat source increases, the sub-critical region is reduced. In all cases the critical value of  $R_z$  decreases with an increasing mass flow ( $M$ ). This demonstrates that increasing the strength of  $M$  destabilises the system.

Figures 4 and 5 explore the variation of the critical values of  $R_z$  with horizontal temperature gradient  $R_x$  for positive and negative values of  $S_z$ , respectively, with different combinations of heat source ( $Q$ ) and the horizontal mass flow ( $M$ ). The linear theory demonstrates that an increase in the horizontal thermal Rayleigh number stabilizes the convection process, however introducing the mass flow in the critical values of  $R_z$  are reduced irrespective of heat source, hence for a fixed  $Q$ , mass flow causes stabilization in the linear case. Even for the non-linear case, in the absence or presence of the heat source and mass flow, increasing the  $R_x$  makes the flow more stable in Fig. 4. When  $S_z$  is negative from Fig. 5 it shows that the linear instability curves are similar to the linear

observations made for positive  $S_z$ . However, this is contradicted in the non-linear results associated with positive  $S_z$  in the presence of  $M$  and  $Q$  at higher values of  $R_x$ . In this case,  $R_z$  decreases as a function of  $R_x$  with increasing mass flow in the medium, and also the flow is stabilised at higher values of  $R_x$  irrespective of  $Q$  and  $M$  seen in Fig. 5. The results indicate that both the linear and non-linear results undergo quantitative changes subject to horizontal thermal and solutal gradients along with the presence and absence of heat source and mass flow variations.

The response of critical values of  $R_z$  as a function of  $Le$  is visualized in Figs. 6 and 7 for positive and negative values of solutal Rayleigh number  $S_z$ , respectively, in the absence and presence of  $M$  at  $Q = 0$ . In the absence of horizontal mass flow (i.e. when  $M = 0$ ) the critical value of  $R_z$  increases as  $Le$  increases and hence the flow become more stable. However, in the presence of  $M$ , the critical value of  $R_z$  is reduced by an increasing  $Le$ . The fall in the critical  $R_z$  in the non-linear theory is further enhanced by increasing  $Le$  as compared to linear theory when  $M$  is present seen for  $S_z > 0$  and  $S_z < 0$ . The regions of potential sub-critical instability are small for  $M = 0$  but increase substantially (as  $Le$  increases) in the presence of mass flow. In both cases for  $S_z = 3$  and  $-3$ , the stability characteristics for linear and non-linear results differ considerably.

## 8 Conclusion

In the present article, we have explored the effect of concentration based heat source on the thermosolutal Hadley convection in porous media in the presence of mass flow, utilising linear and non-linear stability analysis. A comparison between the linear stability thresholds and energy stability thresholds is made by treating the vertical component of the thermal Rayleigh number as an eigenvalue. In both cases the vertical thermal Rayleigh number is evaluated for different combinations of the flow governing parameters. The results indicate the following conclusions:

- In the presence of a mass flow effect, the flow is destabilising in both the linear and

non-linear cases.

- In the presence of a heat source and mass flow, the flow is stabilising at higher horizontal Rayleigh numbers in the linear case, whereas it is destabilizing in the non-linear case at larger mass flows.
- As the concentration based heat source increases, the sub-critical region increases.

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## Nomenclature

$d$	height of porous layer
$D_m$	solotal diffusivity
$g_0$	acceleration due to gravity
$K$	permeability
$k_m$	thermal conductivity
$Le$	Lewis number
$M$	dimensionless mass flow
$P$	dimensionless pressure
$R_x, R_y$	horizontal thermal Rayleigh numbers
$R_z$	vertical thermal Rayleigh number
$S_x, S_y$	horizontal solotal Rayleigh numbers
$S_z$	vertical solotal Rayleigh number
$q$	dimensionless velocity
$Q$	dimensionless heat source
$S$	dimensionless concentration
$t$	dimensionless time
$u, v, w$	$x, y, z$ component of dimensionless velocities

### *Greek symbols*

$\alpha$	dimensionless overall wave number
$\alpha_m$	thermal diffusivity
$(\beta_{\theta_x}, \beta_{\theta_y})$	horizontal thermal gradient vector
$(\beta_{S_x}, \beta_{S_y})$	horizontal solotal gradient vector
$\gamma_\theta, \gamma_S$	thermal and solotal expansion coefficients
$\theta$	dimensionless temperature

$\rho$	density
$\Phi$	porosity
$\xi, \eta$	coupling parameters

*Subscripts*

$f$	fluid region
$m$	porous medium
$s$	steady state

*Superscripts*

*	dimensional variables
'	disturbance quantities

$S_z$	-30	-20	-10	$10^{-5}$	10	20	30
$R_{z_l}$	69.478415	59.478415	49.478413	39.478301	29.478413	19.478414	9.478414
$\alpha_l$	3.141600	3.141600	3.141600	3.141600	3.141600	3.141600	3.141600
$R_{z_e}$	39.478396	39.478396	39.478396	39.478308	29.478411	19.478411	9.478412
$\alpha_e$	3.141600	3.141600	3.141600	3.141600	3.141600	3.141600	3.141600

Table 1

Linear and non-linear case critical thermal Rayleigh number for  $R_x = R_y = S_x = S_y = 0$ ,  $Q = 0$ ,  $M = 0$  and  $Le = 10$ .

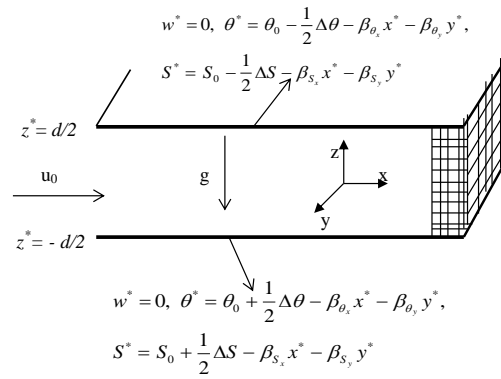


Fig. 1. Schematic diagram of the physical system.

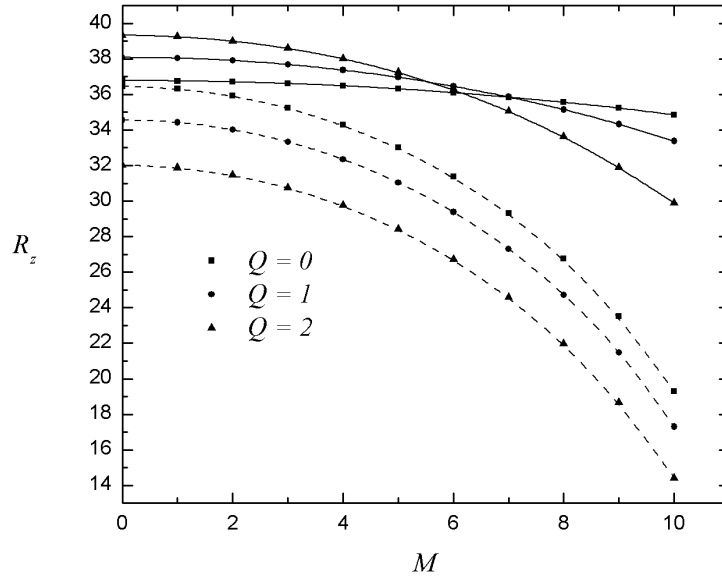


Fig. 2. Variation of  $R_z$  with  $M$  at  $R_x = S_x = 1$  and  $S_z = 3$ .

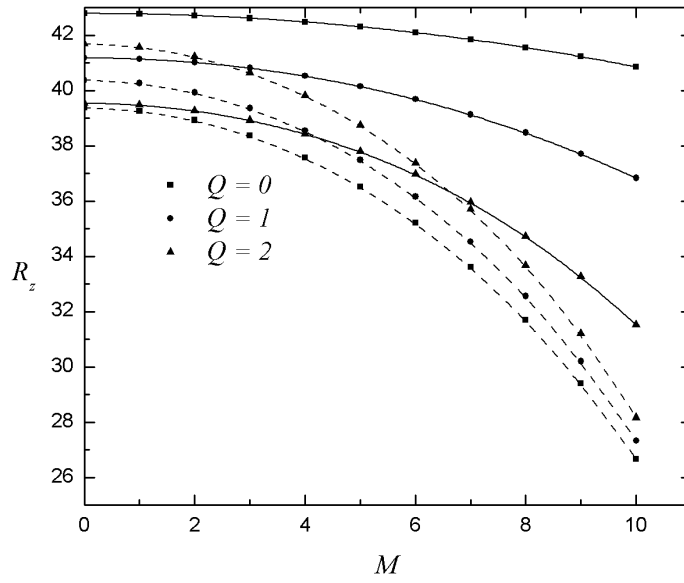


Fig. 3. Variation of  $R_z$  with  $M$  at  $R_x = S_x = 1$  and  $S_z = -3$ .

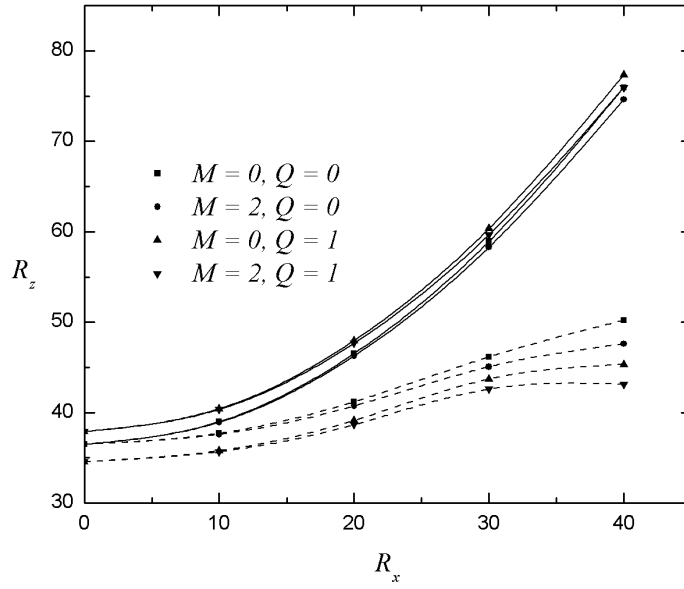


Fig. 4. Variation of  $R_z$  with  $R_x$  at  $Le = 10$  and  $S_z = 3$ .

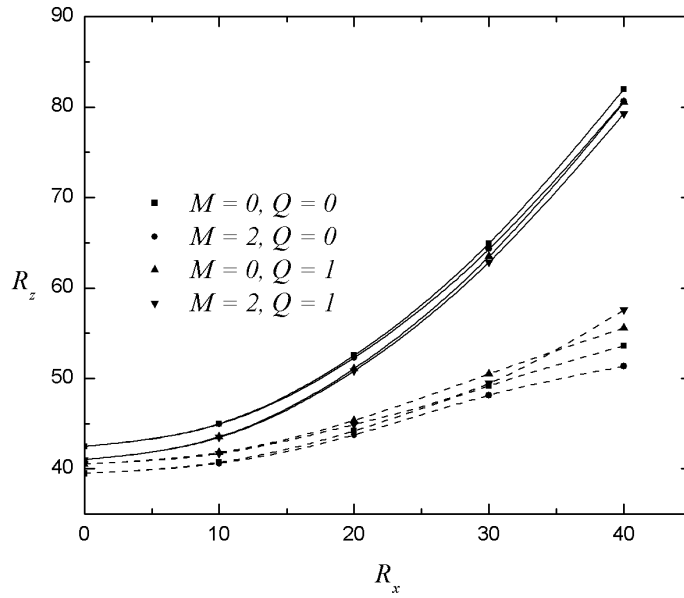


Fig. 5. Variation of  $R_z$  with  $R_x$  at  $Le = 10$  and  $S_z = -3$ .

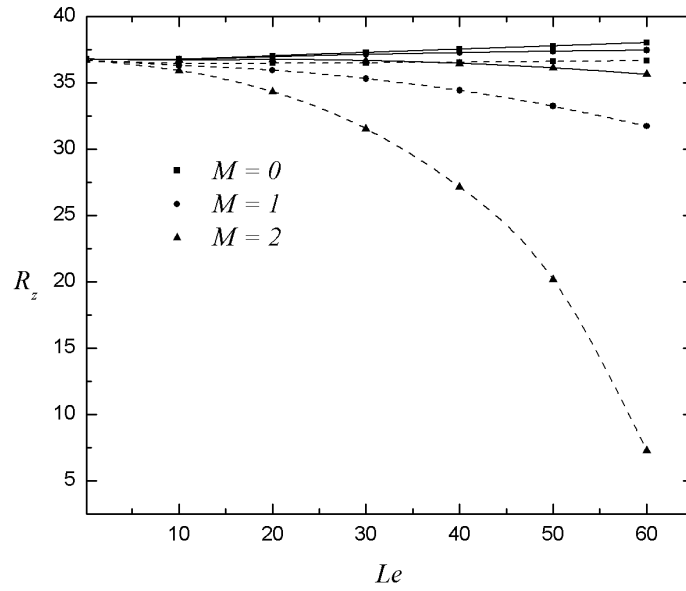


Fig. 6. Variation of  $R_z$  with  $Le$  at  $Q = 0$ ,  $R_x = S_x = 1$  and  $S_z = 3$ .

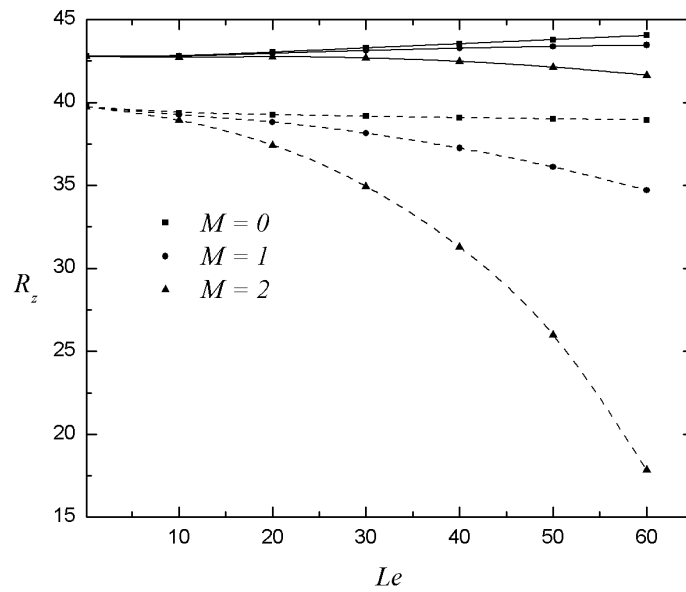


Fig. 7. Variation of  $R_z$  with  $Le$  at  $Q = 0$ ,  $R_x = S_x = 1$  and  $S_z = -3$ .