

1 **Can Whole Building Energy Models Outperform Numerical Models, When** 2 **Forecasting Performance of Indirect Evaporative Cooling Systems?**

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9 **Abstract**

10 This paper presents a whole building energy modelling work incorporating a state-of-the-art
11 indirect evaporative cooling system. The model is calibrated and validated with real-life
12 empirical data, and is capable of representing actual performance of the system with high
13 reliability. The investigated system is a novel super-performance Dew Point Cooler (DPC)
14 with a guideless and corrugated Heat and Mass Exchanger (HMX). The DPC is modelled as
15 part of the whole building energy model through detailed description of system and building
16 characteristics at source code level. The developed model has been simulated in all different
17 climates that an Indirect Evaporative Cooling (IEC) system can be operated, namely:
18 subtropical hot desert, humid continental, Mediterranean, and hot desert climates. The
19 performance predictions has been tested against experiments and numerical model of the
20 same system, and a detailed investigation of modelling approaches to efficiently and
21 effectively model aforementioned systems has been provided.

22 The calibrated and empirically validated whole building energy model predicted the key
23 performance parameters of the dew point evaporative cooling system with mean error values
24 limited to 4.1%. The highest COP values recorded by experiments and whole building
25 energy simulations were 51.1 and 49, respectively. The whole building energy model proved
26 to better predict the performance of dew point evaporative cooler, when compared to
27 numerical models, by incorporating the building-side parameters into the model. This
28 modelling work paves the way toward detailed investigation of the advanced cooling systems
29 within building context to achieve optimised performance of the system in wide range of
30 buildings and operating conditions.

31 **Keywords:** *Dew Point Cooler; Building energy; Model; Performance; Experiment*

32 **1. Introduction**

33 *1.1. Background*

34 The rapid growth in global energy consumption, especially in past decades, has raised the
35 world-wide concern over security of supply as the existing energy resources are exhausting
36 [1]. One of the main contributors to the rising global energy consumption is the service
37 sector which covers all the commercial and public buildings with a wide range of HVAC
38 system [2]. The global energy consumption of service sector has increased by 295 Mtoe in
39 2018 compared to 2000 levels and with this trend the sector would consume a further 323
40 Mtoe by 2040. The sector has also showed the least reduction potential in energy
41 consumption under the Sustainable Development Scenario, compared to Industry,
42 Residential and Transport sectors [1]. To deal with the high energy consumption levels
43 associated with the service sector and to improve its poor performance under future
44 scenarios, the focus has been shifted toward development of advanced, efficient and low-
45 energy HVAC solutions in recent years.

46 The growing energy use by HVAC systems are particularly significant in developed
47 countries. In the USA, HVAC energy use accounts for up to 50% of building energy
48 consumption [3] while in china the HVAC energy use is between 50-70% of the total energy
49 consumed in buildings [4]. Issac and Vuuren [5] estimated that energy demand associated
50 with air-conditioning will rise rapidly in 21st century reaching a peak of 4000 TWh in 2050 and
51 more than 10,000 TWh by 2100. There are other studies which have predicted a similar rise
52 in energy demand of air-conditioning [6] under future weather conditions of USA [7],
53 Switzerland [8], and Australia [9].

54 *1.2. Air-conditioning: past, present and future*

55 Traditionally, the most dominant air-conditioning systems were Mechanical Vapour
56 Compression (MVC) ones which due to their inefficient compressors consumed a
57 considerable amount of electricity [10]. In past decades absorption and adsorption cooling
58 systems have gained more interest over mechanical vapour compression systems due to
59 their lower energy consumption. The absorption and adsorption cooling systems greatly owe
60 their lower energy consumption to replacing energy-intensive compressor with a cycle of
61 high temperature water or vapour which reduces the applicability of these systems in sites
62 with no access to heat source. Complexity of the pressurised and de-pressurised units used
63 in the absorption and adsorption cooling systems and high maintenance costs associated

64 with them are other shortcomings of these systems which have raised the need for practical
65 solutions [11].

66 The most recent approach to provide conditioned air is based on the fundamentals of
67 evaporative cooling which relies on latent heat of water (both recyclable and renewable) to
68 remove dissipated heat from conditioned spaces. The Dew Point Evaporative Cooling
69 approach was first investigated by Dr Valeriy Maisotsenko [12] and the resultant technology
70 is adeptly known as M-cycle cooling [3]. Evaporative cooling systems generally fall under
71 two categories: Direct Evaporative Cooling (DEC) and Indirect Evaporative Cooling (IEC)
72 based on whether the primary air is in direct contact with cooling water or not. In DECs, the
73 direct contact between primary air and cooling water results in production of cooled but more
74 humid air which provides reduced occupant comfort and is not suitable for high-tech facilities
75 like data centres. IECs, on the other hand, separate the primary air and the cooling water by
76 introducing dry and wet channels which cools the product air through the heat transfer
77 between the two channels [13]–[15]. While IECs provide better indoor air quality compared
78 to DECs, they have a lower heat removal capacity due to the constraints introduced by air's
79 wet-bulb temperature.

80 To overcome the shortcomings of IECs, Dew Point Coolers (DPC) as the most advanced
81 indirect evaporative cooling systems available in the market, offer a modified heat and mass
82 exchanger (HMX) configuration to provide pre-cooling for the air in wet channels, eliminate
83 the wet-bulb limits, and lower the product air temperature down to its dew point, thus
84 improving the cooling efficiency by up to 30% compared to conventional IECs [3], [16]–[19].

85 *1.3. Dew Point Coolers*

86 The research on Dew Point Coolers (DPCs) has gained more interest in past decade with
87 first published work dating back to 2006 by Coolerado® project in USA [16] where a cross-
88 flow HMX DPC with perforated holes on the flow path was tested. Results indicated that by
89 employing this type of HMX, for the first time, wet-bulb and dew-point effectiveness of up to
90 80% and 50%, respectively could be achieved under specific operational conditions [16].
91 Since the first successful investigation and implementation of DPCs, more research has
92 considered the potentials of these advanced cooling systems and recorded wet-bulb and
93 dew-point effectiveness has reached values as high as 114% and 84%, respectively by
94 Riangvilaikul et al. [20]. In their study a novel, vertically positioned DPC with counter-flow
95 configuration between the intake and working air, and between the working air and water
96 was tested experimentally.

97 Other example of experimental works on DPCs is a flat-plate cross-flow HMX DPC by Bruno
98 [21] that used a special sheet with high water retention and wicking capability as the wet
99 material layer, and a water-proof membrane as a dry material layer. The authors reported
100 they were able to achieve an average dew-point effectiveness of 75%, which was relatively
101 higher than that of the existing types for the same operational conditions. Xu et al. [4]
102 performed an experimental analysis of a DPC prototype employing a super performance wet
103 material, intermittent water supply configuration and a corrugated HMX to find wet-bulb and
104 dew-point effectiveness of up to 114% and 75%, respectively, and a record-high COP of
105 52.5. The performance of same prototype DPC was then examined by Akhlaghi et al. [22]
106 under four different climatic conditions, namely humid continental, Mediterranean, sub-
107 tropical hot desert, and hot desert climates. Annual energy savings of up to 90% was
108 achieved compared to the conventional MVCs.

109 With increasing demand for even more efficient and low-energy DPCs various modelling
110 techniques and simulation tools have been employed by researchers across the world to
111 investigate complex HMX configurations, water supply patterns, dry and wet channel
112 materials, varying operating conditions and space requirements [20]–[36]. The modelling
113 research on DPCs is investigated critically in the next section with particular attention to
114 experimental validation of model outputs and observed uncertainties, advantages and
115 limitation various modelling approaches introduce, and how this study fills the existing
116 research gap on DPC research topic.

117 *1.4. Modelling DPCs: advantages, limits and the gap*

118 The vast majority of research on DPCs has employed numerical modelling techniques.
119 Hasan [30] employed an analytical model of a regenerative indirect evaporative cooling
120 trying to achieve sub-wet bulb temperature without the need for a vapour compressor. The
121 results of analytical model was compared with a previously developed numerical model and
122 some tests, and the recorded agreement of results ensured validity of system performance
123 modelling [30]. Cui et al. also developed a numerical model of a evaporative dew point
124 cooler [32] and investigated the performance of system under three improved scenarios
125 namely, varying channel dimensions; employing room return air as the working fluid; and
126 installation of physical ribs along the channel length [37]. Their model was validated through
127 comparison of temperature distribution and outlet air conditions with experimental results,
128 and the largest discrepancy was recorded as $\pm 7.5\%$.

129 Lin et al. [33] employed a transient and dynamic numerical model to take into account the
130 dynamic transitions between various components of a DPC and validated the model through

131 inter-model comparison with a steady-state model of the same DPC and experimental
132 comparison which yielded 4.3% discrepancy. Pandelidis et al. performed two numerical
133 studies, one to investigate heat and mass transfer processes in an M-cycle HMX of a DPC
134 [34] and the other to optimize the performance of the same evaporative air cooler [35]. In
135 both studies experimental data was used to ensure the validity of model results and the
136 optimal range of operational and geometrical conditions were identified. Akhlaghi et al. [38]
137 developed a statistical model of a novel DPC employing Multiple Polynomial Regression
138 (MPR) technique to predict the performance of the system. Several operating parameters
139 including intake air temperature, relative humidity and flow rate as well as overall cooling
140 capacity, Coefficient of Performance (COP), and wet bulb efficiency were investigated before
141 applying the model to a number of scenarios in dry climates.

142 Sohani et al. [36] used a Neural Network (NN) based numerical model to study and optimise
143 the performance of a DPC with M-cycle under 12 diverse climatic weather conditions. While
144 the multi-objective optimisation technique used by authors was able to improve mean values
145 of the COP and cooling capacity by 8.1% and 6.9%, adequate evidence on empirical
146 validation of the model was not provided. Chen et al. [24] employed a experimentally
147 validated numerical model of an IEC to perform a detailed sensitivity analysis and
148 optimisation based on the most influential and practically controllable parameters. Xu et al.
149 [28] also did a numerical modelling work on guideless irregular HMX with corrugated heat
150 transfer surface as used in a novel DPC. The experimentally validated work proved that the
151 novel DPC system was capable of achieving up to 37% more cooling capacity, 55.8% higher
152 wet bulb efficiency, and 33.3% higher COP.

153 Other studies by Moshari and Heidarnejad [23], Akhlaghi et al. [39], [22], Riangvilaikul [20],
154 [26], and Jradi et al. [27] all performed some sort of numerical modelling exercise in IECs
155 and validated their findings through comparison with experimental data and other models.
156 While all these studies were successful in recording some or extraordinary improvements in
157 performance of the investigated systems, the vast majority of improvements were recorded
158 under controlled test conditions in laboratory environment, neglecting the extensive building
159 and occupants' interactions which happen in real world.

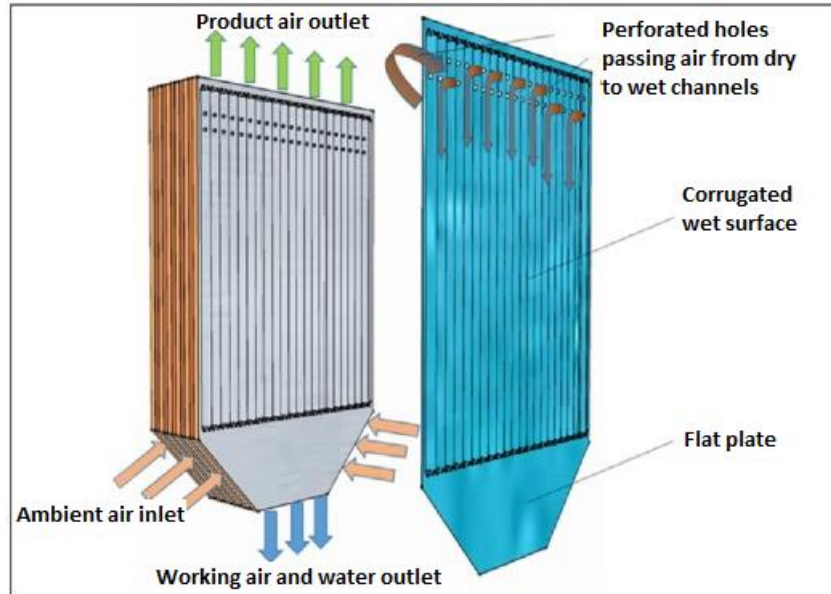
160 This study, therefore, fills the existing gap in DPC research by investigating the performance
161 of a novel dew point evaporative cooling system through whole building energy modelling
162 where the restraining system interactions with hosting building and its occupants are
163 captured. In this way the transient behaviours of the system within the building envelope are
164 quantified and the resultant impact on performance parameters of the system is investigated.
165 A comparison of the predicted performance parameters from whole building energy

166 simulation to those from numerical models of the same system enabled the critical
167 assessment of each modelling approach in dealing with advanced Indirect Evaporative
168 Cooling (IEC) systems.

169 **2. System Description**

170 This study investigates a state-of-the-art, high-performance counter flow DPC employing a
171 complex, 4 kW rated Heat and Mass Exchanger (HMX). The new HMX configuration
172 replaces the channel support guides with a corrugated heat transfer surface separating dry
173 and wet channels (as depicted in **Figure 1**) which decreases air flow resistance by up to
174 56% and increases heat transfer area by up to 40% leading to an improved heat transfer
175 rate [28]. As seen in Figure 1 (a), a number of perforated holes are designed on top of each
176 corrugated sheet to allow partial flow of air from dry channels to wet ones in order to
177 complete heat transfer cycle and cool down the air in dry channels. The dry channels are
178 made of a specific aluminium with high malleability while the wet channels' material is a
179 flexible *Coolmax*[®] fibre with high water absorption, diffusion and evaporation capacities
180 which allows the sheet to have corrugated shape. The geometric dimensions of the HMX is
181 summarised in **Table 1**.

182 When system operates, the air with relatively high temperature and moisture level enters the
183 DPC and passes through the dry channel losing its heat to the adjacent wet channel
184 reducing its temperature to the desired level. Upon reaching the end of dry channel a part of
185 cooled air leaves the channel as product air (to the conditioned space) and the remaining air
186 is transferred to the wet channels through perforated holes as working air. This working air
187 then gains heat from adjacent dry channel and moisture from *Coolmax*[®] material while
188 passing through the wet channel and is discharged as exhaust air and water drops. In
189 comparison to conventional flat plate HMXs, the introduced HMX configuration reduces the
190 airflow resistance, increases heat transfer area, has higher diffusion area and better
191 evaporation owing to use of *Coolmax*[®] wet channel material.



192 **Figure 1** Heat and Mass Exchanger (HMX). Upper: configuration and structure, Lower:
 193 corrugated heat transfer surfaces separating dry and wet channels [38]

194 Owing to the high absorption capacity of fibrous material in the wet channels, the intermittent
 195 water supply scheme was used by a dedicated water distributor system, which reduces the
 196 amount of water used as well as water pump power consumption. The water distributor is
 197 composed of a water pump, a water header, a water sink, and a water distributor tubes
 198 which enable the even distribution of water over the surface of wet channels. When the
 199 water sink underneath the HMX is empty, the water is supplied with flow rate of 6.85 L/min
 200 for 15 seconds with 10 minutes intervals, and when the tank is full, the water is supplied with
 201 flow rate of 2.45 L/min for 60 seconds with 10 minutes intervals.

202 In addition to the complex HMX introduced above, the DPC also employs two supply and
 203 two exhaust air fans each with 160 W power, 458 Pa pressure, and 705 m³/h volumetric flow
 204 rate, one circulating water pump with 24V DC power and 450 L/h flow rate, and two

205 controllers for the fans and the water pump. **Table 2** summarises the key elements of the
 206 DPC system and associated technical specifications.

207 **Table 1** Geometric dimensions of the Heat and Mass Exchanger

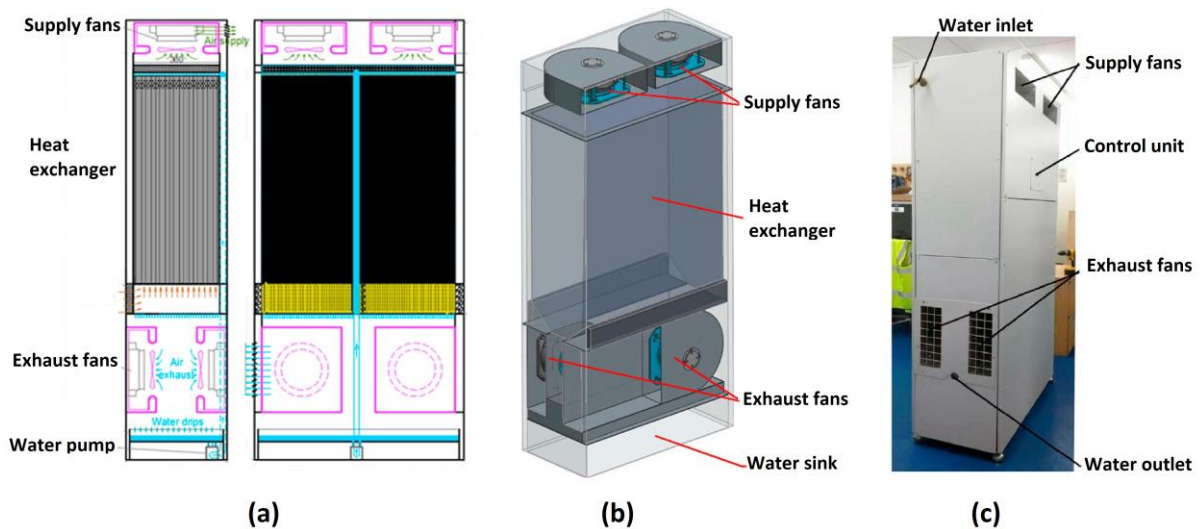
Inlet flat plate height	120	mm
Outlet flat plate height	10	mm
Corrugated plate height	860	mm
Transition length between flat and corrugated plates height	5*	mm
Number of corrugated plates	160	-
Total height of the HMX	1000	mm
Width	800	mm
Length	358	mm
Total heat transfer area	49.3	m ²
Height of corrugated wave	2.8	mm
Width of corrugated wave	11.6	mm

*on each of the inlet and outlet sides

208 **Table 2** Technical manufacturer specifications of the DPC components

Component	Specifications
Supply air fan	R3G225-RE07-03, ebm-papst Ltd, fan speed 2865 rpm, 705 m ³ .h ⁻¹ , 458 Pa, 160 W
Exhaust air fan	R3G225-RE07-03, ebm-papst Ltd, fan speed 2865 rpm, 705 m ³ .h ⁻¹ , 458 Pa, 160 W
Water pump	DH40H-24110, Shenzhen Zhongke Century Technology, 24 V/1.2 A DC, 11mH ₂ O, 450 L/hr
Fan controller	980-CAS11007 – TMS Controller, ebm-papst Ltd
Pump controller	DH48S-S, Xinling Electrical Co. Ltd

209 **Figure 2** represents the whole system design, the computer model, and the actual system in
 210 the laboratory environment.



211

(a)

(b)

(c)

212 **Figure 2** Dew Point Cooler (DPC) and its components. (a): 2D cross-section view, (b) 3D
 213 computer model, (c): actual system in the lab environment [4]

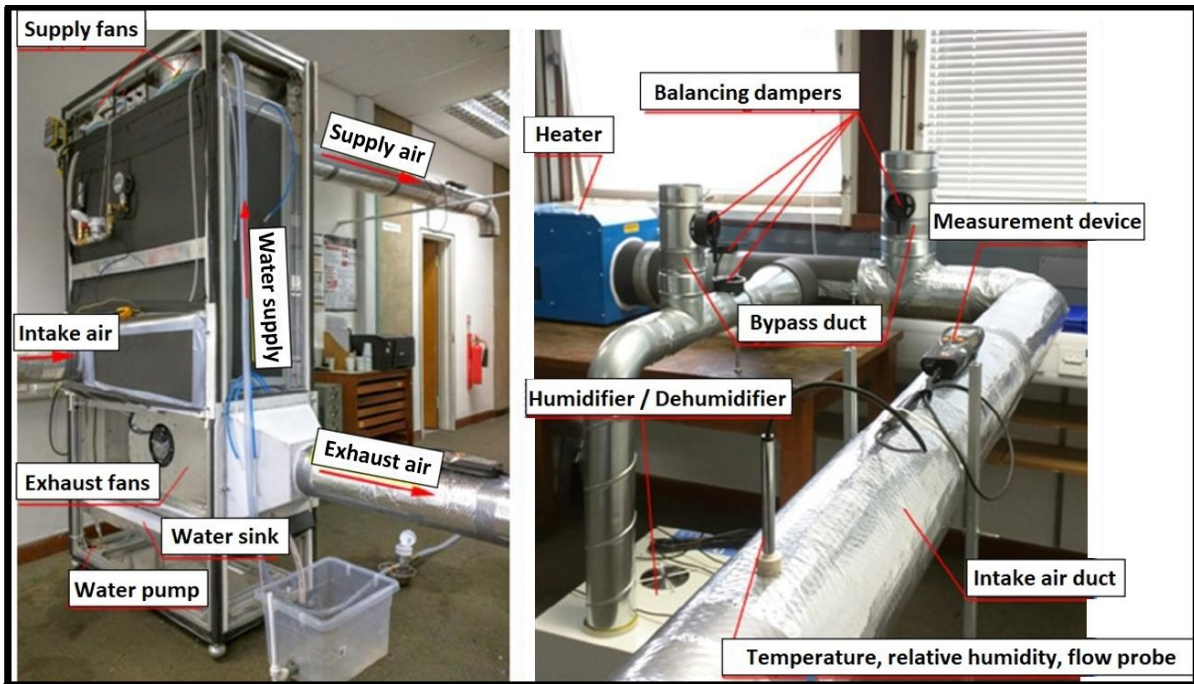
214 Finally, for optimum operation of the DPC, temperature of the running water is kept at the
 215 range of 16-20°C to ensure efficient cooling [4]. A water filter with cartridge to purify the
 216 water and an anti-scale agent was used to minimise the risk of blockage at the perforated
 217 holes. Also an optimised water distribution scheme was introduced to maximise the use of
 218 circulating water within the cooler and reduce the amount of intake water [4].

219 3. Experimental Set-up and Analysis Method

220 To examine performance of the novel 4 kW Dew Point Cooler (DPC) with introduced
 221 complex Heat and Mass Exchanger (HMX), the test set-up presented in **Figure 3** was
 222 constructed in the lab environment. The test set-up comprises a heater, a
 223 humidifier/dehumidifier, and four balancing dampers to enable conditioning of the inlet air
 224 and simulate various weather conditions.

225 The water pump, supply and exhaust fans, and supply-discharge ducting system is also
 226 presented in **Figure 3**. After conditioning the inlet air temperature and humidity to match
 227 those of the climates under study, the supply fans and the necessary ducting is used to
 228 create a zero static pressure at the inlet of DPC. A specific multi-function measurement
 229 device capable of measuring the ventilation and air conditioning parameters as well as
 230 indoor air quality parameters (i.e. temperature, humidity, flow rate and speed) was used to
 231 identify the characteristics of the air flow at the inlet and outlet of the system. The
 232 measurement points were placed at a distance 10 times the diameter of the ducts ($\phi 160$
 233 mm) from inlet and outlet of the system to allow development of fully steady air flow for the
 234 sake of accuracy of measurements. Two water flow meters were also installed at the inlet

235 and outlet of wet channels to measure the amount of water used and consequent pressure
 236 drop. A water pressure of 1.8 mH₂O was preserved throughout the system to ensure even
 237 distribution of the water across the wet surfaces (as suggested by *Coolmax*[®] wet channel
 238 material manufacturer). Finally, a simple fan controller was employed to achieve the
 239 optimum working air to intake air ratio of 0.37, and product air and waste air flow rates of 602
 240 m³.h⁻¹ and 364 m³.h⁻¹, respectively, throughout the experiments as identified by [20].



241

242 **Figure 3** Experimental test set-up with individual components as constructed in the
 243 laboratory environment

244 The measure parameters from the system are recorded in real time and analysed to quantify
 245 the overall cooling capacity, Coefficient of Performance (COP), wet bulb and dew point
 246 efficiencies. The overall cooling capacity of the system can be calculated from **Equation 1**,
 247 as suggested by ASHRAE [40] for all Indirect Evaporative Cooling (IEC) systems:

$$Q_{Cooling} = C_p(T_{dry,in} - T_{dry,out})(1 - \varphi)Q_{m,dry,in} \quad \text{Equation 1}$$

248 Where $Q_{Cooling}$ is the cooling capacity of DPC, C_p is the specific heat capacity of the inlet
 249 air, $T_{dry,in}$ and $T_{dry,out}$ are the inlet and outlet temperatures of the air in dry channel, φ is
 250 the working air to intake air ratio, and $Q_{m,dry,in}$ is the mass flowrate of the intake air in the
 251 dry channel.

252 Then the Coefficient of Performance (COP) can be calculated as the ratio of cooling capacity
253 to the total of electrical power consumed by fans (W_{Fans}) and pumps (W_{Pumps}):

$$COP = \frac{Q_{Cooling}}{W_{Fans} + W_{Pumps}} \quad \text{Equation 2}$$

254 Finally, the wet bulb and dew point efficiencies (ε_{wb} and ε_{dp}) are calculated from **Equation 3**
255 and **Equation 4**, respectively:

$$\varepsilon_{wb} = \frac{T_{dry,in} - T_{dry,out}}{T_{dry,in} - T_{dry,in,wb}} \quad \text{Equation 3}$$

$$\varepsilon_{dp} = \frac{T_{dry,in} - T_{dry,out}}{T_{dry,in} - T_{dry,in,dp}} \quad \text{Equation 4}$$

256 Where $T_{dry,in,wb}$ and $T_{dry,in,dp}$ are the wet-bulb temperature of the intake air in dry channel
257 and the dew point temperature of the intake air in dry channel, respectively.

258 Having identified the performance parameters needed to investigate the DPC, four
259 representative cities with totally different weather conditions were identified to test the
260 performance of system. These cities are: Las Vegas (USA) with subtropical hot desert
261 climate, Beijing (China) with humid continental climate, Rome (Italy) with Mediterranean
262 climate, and Riyadh (KSA) with hot desert climate. The weather conditions from these cities
263 were simulated and corresponding intake air with representative temperature and humidity
264 levels were produced in the laboratory environment to test the performance of DPC under
265 each climate. Due to very high relative humidity of the air in Beijing and Rome, a pre-
266 treatment had to been applied to the intake air in order to bring the humidity level to the
267 operational range (<40%) of the DPCs in common high-tech facilities like data centres [39].
268 Hence, this research could focus solely on the cooling performance of the system without
269 having to take into account the dehumidification. The dehumidification process was carried
270 out using a solar/waste energy driven dehumidification cycle employing a desiccant bed
271 located inside a channel that is constructed by a porous and visible-light LiCl-Silicon-Gels
272 material. As a result of the dehumidification process, the moisture content of outside air in
273 Beijing and Rome are brought down required range resulting in a parallel sensible cooling
274 process. The monthly average temperature and relative humidity of the four representative
275 cities and corresponding pre-treated values for Beijing and Rome are all summarised in
276 **Table 3**.

277 As seen in **Table 3** the temperature and humidity values are given only for the months where
 278 free cooling is not available in each particular climate and there is need for operation of
 279 DPC. The average outdoor temperature required for free cooling is identified as 22°C based
 280 on ASHRAE guidelines for power requirements in data centre design [41]. For Beijing and
 281 Rome weather conditions where pre-treatment was necessary, the pre-treated monthly
 282 temperatures are taken as the selection criteria. Hence, the DPC operation is required from
 283 March to October in Riyadh, from April to October in Beijing and Las Vegas, and from May to
 284 October in Rome as seen in **Table 3**.

285 **Table 3** Monthly average temperature and humidity values for the four representative cities
 286 with pre-treatment data where required

Month	Beijing				Rome				Las Vegas		Riyadh	
	Before pre-treatment		After pre-treatment		Before pre-treatment		After pre-treatment		No pre-treatment needed			
	T(°C)	RH	T(°C)	RH	T(°C)	RH	T(°C)	RH	T(°C)	RH	T(°C)	RH
March	-	-	-	-	-	-	-	-	-	-	27	37%
April	20	45%	23.7	16%	-	-	-	-	25	25%	31	35%
May	26	53%	30.8	23%	23	75%	27.3	39%	30	21%	38	21%
June	30	60%	35.6	24%	26	74%	30.8	35%	37	18%	42	16%
July	31	75%	36.8	24%	28	73%	33.2	38%	40	20%	44	17%
August	30	78%	35.6	40%	28	75%	33.2	39%	39	27%	42	19%
September	27	69%	32	35%	27	75%	32	39%	33	26%	42	19%
October	20	60%	23.7	28%	23	76%	27.3	40%	27	30%	35	23%

287 Having identified the intake air properties, the heater and humidifier/dehumidifier shown in
 288 **Figure 3** were used to produce the intended intake air for the DPC and then the DPC was
 289 operated under each weather conditions. The system performance parameters as well as
 290 the achieved indoor air properties were recorded and are presented in **Section 6**.

291 **4. Numerical Model of the System**

292 A numerical model of the advanced Dew Point Cooler (DPC) with corrugated HMX design
 293 was developed using Multiple Polynomial Regression (MPR) technique [38]. Regression
 294 analysis is a very popular and well know method as it provides robust grounds for
 295 developing predictive tools to investigate complex relations between dependant and

296 independent parameters in a wide range of areas i.e. engineering, physics and chemical
 297 sciences [42], [43]. The developed model takes a set of operational and geometric
 298 parameters as input to predict the performance parameters of the DPC under investigation.
 299 These parameters and their corresponding ranges as used in the MPR model are
 300 summarised in **Table 4**.

301 **Table 4** Operational and geometrical parameters used in the MPR model to predict
 302 performance parameters of the DPC and the corresponding ranges

Operational Parameters	Range	Geometrical Parameters	Range	Performance Parameters
Intake air temperature, T(°C)	25-45	Channel height, H (m)	1-3	Cooling capacity
Intake air relative humidity, RH	0.125-0.5	Channel interval, Int (m)	0.004-0.008	Coefficient of Performance
Intake air flow rate, U (m/s)	0.3-3.3	Number of layers, L	100-200	Dew point effectiveness
Working air to intake air ratio (φ)	0.1-0.9	-	-	Wet-bulb effectiveness

303 The operating and geometrical parameters were used as independent parameters in the
 304 MPR model mainly due to the flexibility of these parameters which allows them to be
 305 changed continuously in real-life operation of the DPC. Hence, other parameters which didn't
 306 offer such flexibility were excluded from input parameters of the model.

307 **Table 5** Discrete values selected for operating parameters to construct training and
 308 validation sets of the MPR model [38]

No	Training set				Validation set			
	T (°C)	RH	U (m/s)	φ	T (°C)	RH	U (m/s)	φ
1	25	0.125	0.3	0.1	26.25	0.14	0.5	0.15
2	27.5	0.17	0.7	0.2	28.75	0.19	0.9	0.25
3	30	0.22	1.1	0.3	31.25	0.24	1.3	0.35
4	32.5	0.26	1.5	0.4	33.75	0.28	1.7	0.45
5	35	0.3	1.9	0.5	36.25	0.32	2.1	0.55
6	37.5	0.34	2.3	0.6	38.75	0.36	2.5	0.65
7	40	0.38	2.7	0.7	-	-	-	-
8	42.5	0.42	3	0.8	-	-	-	-
9	45	0.5	3.3	0.9	-	-	-	-

309 Having identified the input (operational and geometrical) parameters and their ranges,
310 discrete values for each parameter were required to construct a training set to develop the
311 model and a validation set to verify the developed model. Hence, 9 discrete values for the
312 training set and 6 discrete values for the validation set were selected to develop the MPR
313 model (**Table 5**).

314 As seen in **Table 5** the discrete values for the two sets were chosen such that the validation
315 set values won't overlap with training set values, hence offering robust model validation
316 grounds. As for geometrical parameters, discrete values of 1m, 2m, and 3m for height,
317 0.0004m and 0.008 for interval, 100 and 200 for number of layers were used in the model
318 (see **Figure 1** for geometrical parameters). Water temperature was modelled as 16°C and
319 water flow rate as 411 L/h to match the experimental values [4]. All the possible
320 combinations with these discrete values were considered in the model to account for all the
321 random operating conditions. Hence, the total number of operating conditions becomes 7857
322 in which 80% of them, 6561 (9⁴), are for training set and 20%, 1296 (6⁴), are for the
323 validation set. Once the model is developed and validated, it can be used beyond the scope
324 of the discrete values and ranges presented in **Table 4** and **Table 5**.

325 The regression model was developed from the described data sets in R software package
326 can be represented in the following equation:

$$\begin{aligned} Y = & \beta_0 + \beta_1 \times (T^{n_{1,1}} \times RH^{n_{2,1}} \times U^{n_{3,1}} \times \varphi^{n_{4,1}}) \\ & + \beta_2 \times (T^{n_{1,2}} \times RH^{n_{2,2}} \times U^{n_{3,2}} \times \varphi^{n_{4,2}}) + \dots \\ & + \beta_m \times (T^{n_{1,m}} \times RH^{n_{2,m}} \times U^{n_{3,m}} \times \varphi^{n_{4,m}}) \end{aligned} \quad \text{Equation 5}$$

327 Where Y represents all the performance parameters to be predicted by model, T is
328 temperature, RH is the relative humidity, U is air flow velocity of intake air, and φ is the
329 working air to intake air ratio. $\beta_0, \beta_1, \beta_2, \dots, \beta_m$ are regression coefficients to represent
330 geometric characteristics; $n_{1,m}$ represents the intake air temperature of the m^{th} coefficient,
331 $n_{2,m}$ represents intake air humidity of the m^{th} coefficient, $n_{3,m}$ represents intake air flow
332 velocity of the m^{th} coefficient, and $n_{4,m}$ represents the working air to intake air ratio of the m^{th}
333 coefficient.

334 The model was developed based on the introduced training sets and the validation set was
335 used to verify the predicted performance parameters (Y). For validation purpose, least
336 squares method was used where the sum of squared residuals are minimised. The residual
337 or Sum Square of Errors (SSE) is the difference between the actual values and the
338 estimated regression values by MPR model (also denoted as r_i):

$$SSE = \sum_{i=0}^N (\hat{Y}_i - Y_i)^2 = \sum_{i=0}^N r_i^2 \quad \text{Equation 6}$$

339 Where \hat{Y} represents the predicted value of individual performance parameters, Y is the
 340 actual value of the same parameter, and N is the number of predicted value. Having
 341 identified the SSE value, three of the main metrics to evaluate the performance of the model
 342 i.e. Mean Square Error (MSE), Maximum Relative Error (MRE), and coefficient of
 343 determination (R^2) can be calculated:

$$MSE = \frac{SSE}{N} = \frac{\sum_{i=0}^N (\hat{Y}_i - Y_i)^2}{N} = \frac{\sum_{i=0}^N r_i^2}{N} \quad \text{Equation 7}$$

$$R^2 = 1 - \frac{SSE}{SST} = 1 - \frac{\sum_{i=0}^N (\hat{Y}_i - Y_i)^2}{\sum_{i=0}^N (\bar{Y}_i - Y_i)^2} \quad \text{Equation 8}$$

344 Where SST is sum square of total, and \bar{Y} is the mean of predicted values.

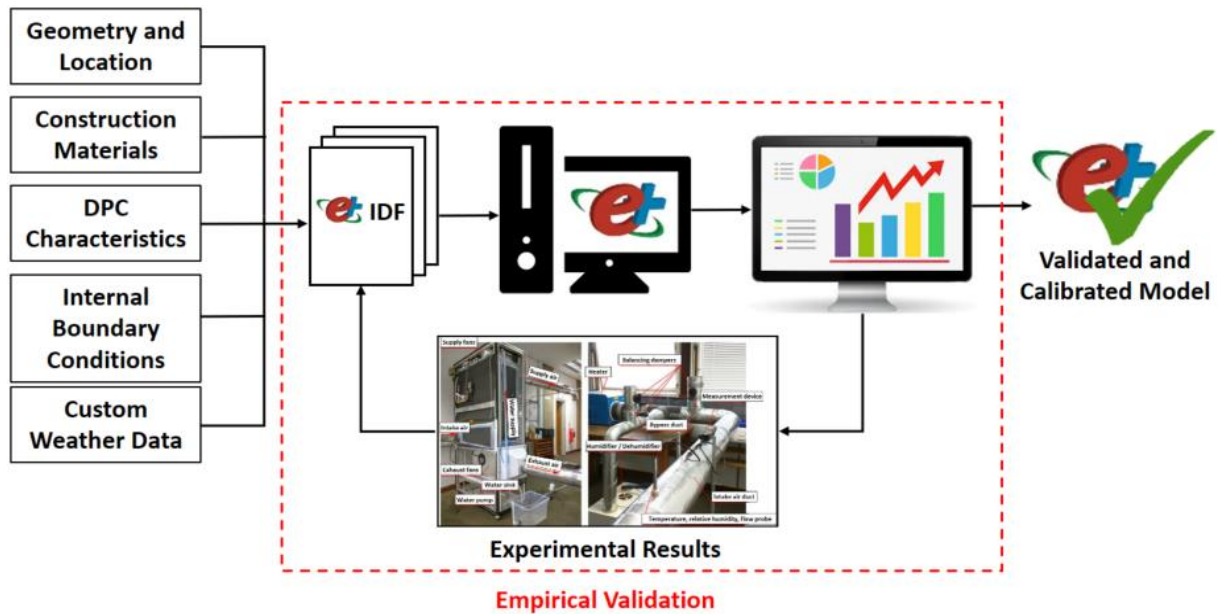
345 5. Whole Building Energy Model

346 The whole building dynamic energy model of the system and the hosting building was
 347 developed using EnergyPlus (e+) software package (version 8.9.0.1) [44], which is open
 348 source, widely used and verified. In order to enable empirical validation and comparison with
 349 numerical model, the same system parameters and numerical model inputs as described in
 350 **Sections 2, 3 and 4** were used in developing the whole building energy model. Where there
 351 was lacking data, further data collection was conducted to create a detailed energy model
 352 which is capable of representing reality with high reliability.

353 To facilitate the data input process, DesignBuilder [45] software version 6.1.2.009 was
 354 employed to create laboratory building's geometry (where DPC was operated and tested),
 355 construction materials, internal boundary conditions and a template of an Indirect
 356 Evaporative Cooler (IEC). DesignBuilder was used initially because it is a commercially
 357 available software package that offers detailed dynamic thermal simulations, employing the
 358 EnergyPlus simulation engine and provides a user friendly graphical user interface [45].

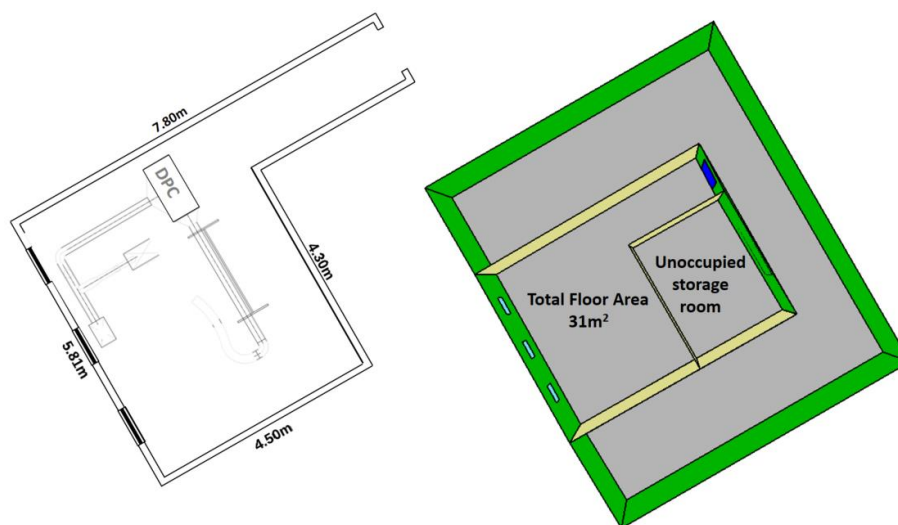
359 Having formed the basis for energy model of the DPC in Laboratory environment, the
 360 corresponding EnergyPlus Input Data File (IDF) was exported with *.idf* extension. The IDF
 361 was then modified using a text editor and the EnergyPlus IDF editor [46] to add exact DPC
 362 characteristics as described in **Sections 2 and 3 (Figure 4)**. The completed IDF with custom
 363 weather files created for the four cities investigated in the experiments (see **Table 3** for

364 details) were fed to the EnergyPlus and simulations were run. As seen in **Figure 4** the
 365 simulation results were then checked against experimental results and necessary
 366 modification were added to the EnergyPlus IDF in order to produce the validated and
 367 calibrated model of the DPC under investigation.



368
 369 **Figure 4** Schematic of the whole building energy modelling process: from raw data to the
 370 validated model

371 Upon completion of the modelling process as depicted in **Figure 4**, the validated whole
 372 building energy model and the performance parameters predictions are compared to the
 373 numerical model estimates (**Section 6**).



374
 375 **Figure 5** Left: Floor plan of the laboratory room depicting DPC configuration, Right: Building
 376 layout with adjacent rooms to the laboratory as modelled in DesignBuilder

377 The building hosting the Dew Point Cooler (DPC) in experiments was modelled in
378 EnergyPlus software package based on the data collected through a comprehensive survey
379 carried out on the building. **Figure 5** presents the floor plan of the laboratory building with
380 DPC test set-up, and a 2-D view of the building model.

381 As seen in **Figure 5** the adjacent spaces to the experiment room is also modelled in order to
382 capture possible impact they can have on the indoor environment of the laboratory and
383 consequently on system performance. The experiment room has total floor area of 31m^2 and
384 floor to ceiling height of 2.7m with an L-shaped layout, three windows with total glazing area
385 of 1.1m^2 and a wooden entrance door with area of 1.6m^2 . **Table 6** summarises the
386 construction materials of the building, their compositions and their corresponding U-values
387 as modelled in EnergyPlus. Since the construction details of the building wasn't a part of
388 analysis in previous experimental or numerical modelling studies, the required details for
389 developing the whole building energy model was gathered separately by surveying the
390 building envelope and referring to building plans and construction handbook provided by
391 states office at the University of Hull, where the DPC is tested. Hence, the description of
392 construction materials and details of their layers were used in the modelling process and
393 resultant U-values are reported in **Table 6**.

394 The external walls are made of lightweight concrete blocks as outermost layers followed by a
395 thin air gap and plasterboard on the inside of the building, with an overall U-value of 1.6
396 $\text{W}/\text{m}^2\text{K}$. The laboratory where the experiments were carried out was located on second floor
397 of the building, hence the internal floor and ceiling was modelled as a solid concrete slab
398 with U-value of $0.7 \text{W}/\text{m}^2\text{K}$. The room has three square windows, equally spaced on the
399 external wall with single glazing and aluminium frame which were closed during the
400 experiments and hence modelled with zero opening area and overall U-value of $4.8 \text{W}/\text{m}^2\text{K}$.
401 The entrance door to the room was a wooden one with 65mm thickness and U-value of 3.0
402 $\text{W}/\text{m}^2\text{K}$. Finally, the internal partitions separating the experiment room from the rest of
403 building were formed of a single layer brickwork covered with plaster on each side giving the
404 walls a thickness of 220mm and U-value of $2.1 \text{W}/\text{m}^2\text{K}$.

405 Measuring infiltration rates of the experiment room was not possible at the time of this study
406 as the tests were running in the experiment room. Instead, airtightness test results of a
407 similar laboratory in the same building which was carried out in 2017 and reported in building
408 data repository was used. The airtightness test was carried out with 50 Pa pressurised unit
409 and **Equation 9**, from BS EN 12831 [47] was used to convert the reported value to
410 infiltration rate at normal operating conditions:

$$\dot{V}_{inf,i} = 2 \times V_i \times n_{50} \times e_i \times \varepsilon_i \quad \text{Equation 9}$$

411 Where $\dot{V}_{inf,i}$ is the infiltration rate of the space, V_i is the volume of space (m^3), n_{50} is the air
 412 exchange rate per hour (ACH), resulting from a pressure difference of 50 Pa between the
 413 inside and outside of the building, e_i is the shielding factor which was taken as 0.03 for a
 414 moderate shielding and heated spaces with more than one exposed opening, and ε_i is
 415 height correction factor which takes into account the increase in wind speed with the height
 416 of the space from ground level. $\varepsilon_i = 1$ when the centre of zone height to ground level is
 417 below 10m which was the case in the experiment room. Inserting the infiltration value of 0.16
 418 ACH (as result of airtightness test) into the **Equation 9**, an infiltration rate of 0.8 ACH was
 419 calculated and added to the whole building energy model of the building.

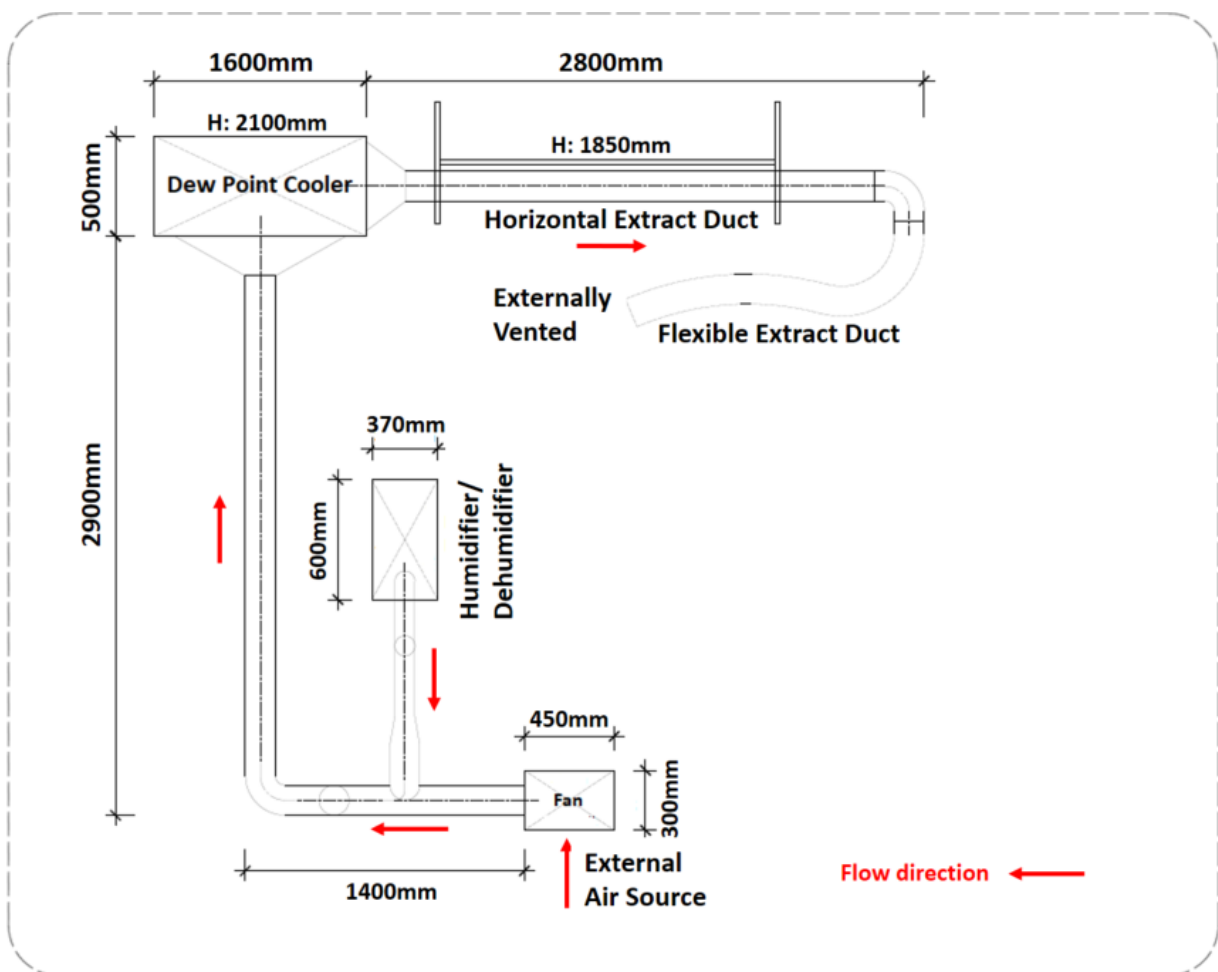
420 **Table 6** Summary of construction materials as modelled in EnergyPlus, physical properties,
 421 and corresponding overall U-values

Element	Description	Layers	Thickness (mm)	Density (kg/m ³)	Specific heat capacity (J/kgK)	U-value (W/m ² K)
External walls	Lightweight concrete block, air gap and plasterboard	Concrete block	200	600	1000	1.6
		Air gap	25	-	-	
		Steel	10	7800	450	
		Plasterboard	10	900	1000	
Internal floor/ceiling	Solid (concrete slab)	Cast concrete	150	2100	840	0.7
Windows	Single glazing with aluminium frame	Glazing	3	-	-	4.8
		Frame	35	2800	880	
Entrance door	Wooden	Painted oak	65	700	2390	3.0
Internal partitions	Solid Brick	Brick (inner)	220	1700	1000	2.1

422 The building was modelled as two thermal zones: the experiment room and the rest of the
 423 building. The heat gains from the system equipment were excluded from the zone definition
 424 as these details are included in the system model and the resultant impact on system
 425 performance and indoor environment is considered. The occupancy and the metabolic gains
 426 are also modelled to represent presence of a single person (to run the experiments) in the
 427 room during system operations and no window or door opening is considered to eliminate
 428 the impact of external air flow on system performance. Lighting gains of 10 W/m² are also
 429 considered in the model.

430 The custom EnergyPlus weather files were created by scaling typical weather year data from
 431 the International Weather for Energy Calculations (IWEC) [48] following the methodology
 432 described in a previous article by the authors [49]. Monthly values of external air temperature
 433 and relative humidity were compared with the experimental weather values to produce a
 434 scaling factor. The scaling factor was then applied to the hourly values using EnergyPlus
 435 auxiliary weather programme [46] to produce equivalent weather information suitable for
 436 whole building energy modelling. For weather information from Beijing and Rome, the pre-
 437 treated values given in **Table 3** were used to develop the equivalent hourly weather file,
 438 whereas for Riyadh and Las Vegas the original values were used as no pre-treatment was
 439 found necessary.

440 The DPC was modelled explicitly in EnergyPlus by detailed modification of the IDF's
 441 including geometry and construction details. The dimension and size details of the system,
 442 as presented in **Figure 6**, were added into IDF's as object-oriented entries which sat in the
 443 previously allocated lines of the IDF as assigned by the system template.



444

445 **Figure 6** Dew Point Cooler (DPC) and test set-up technical plan as constructed in laboratory
 446 environment with component dimensions

447 The overall power requirements of the pumps and fans (90.5 W), pressure rise range and
448 efficiencies as identified in product catalogues, air flow rates passing through the wet and
449 dry channels of the DPC as measured in the experiments (602 and 364 m³.h⁻¹), and height
450 of air inlets (2.1m) and outlets (1.85m) as depicted in **Figure 6** were all included the IDF's to
451 ensure system model is capable of simulating real-life operation of the DPC.

452 The details of the system as constructed in the laboratory environment was input explicitly
453 into IDF's except for the Thermal Mass Parameter (TMP). This was due to EnergyPlus not
454 having the capacity to model system physically, instead the operation and performance of
455 the system was modelled. Hence, the experiment room was modelled as a vacant space
456 with conditioned air inlet and exhaust air outlets. To account for the TMP of system
457 component, a further TMP of 50 kJ/m²K was added to the existing TMP of the building as
458 calculated from **Equation 10** [50]:

$$TMP = \frac{\sum \kappa \times A}{TFA} \quad \text{Equation 10}$$

459 Where κ is the heat capacity (kJ/m²K) of each element, A is the element's area, and TFA is
460 the Total Floor Area of the experiment room, and the summation is over all walls together
461 with both sides of all internal walls and floors/ceilings.

462 **6. Results and Discussion**

463 *6.1. Comparison of the whole building energy model results with experiments:* 464 *empirical validation*

465 The completed IDF's which were developed to represent the actual system and hosting
466 building's characteristics under equivalent experimental conditions were fed to the
467 EnergyPlus calculation engine and simulations were run for the previously identified climates
468 (see **Table 3** for climate details). The model was calibrated and simulations were compared
469 to experimental results in order to validate the model. All the simulations were run in
470 EnergyPlus version 8.9.0.1, and simulation of system operation under each climate required
471 approximately 18 minutes of single CPU time for a full year simulation at 1-minute time
472 steps. The model was calibrated using the operational parameters contributing to cooling
473 capacity of the system, as provided in **Equation 1**. The specific heat capacity of the inlet air
474 (C_p), the inlet and outlet temperatures of the air in dry channel ($T_{dry,in}$ and $T_{dry,out}$), and the
475 working air to intake air ratio (φ) as modelled in EnergyPlus were checked against
476 experimental values to ensure system model characteristics matched those of the actual
477 system. Having calibrated the system model, simulation results were exported and analysed.

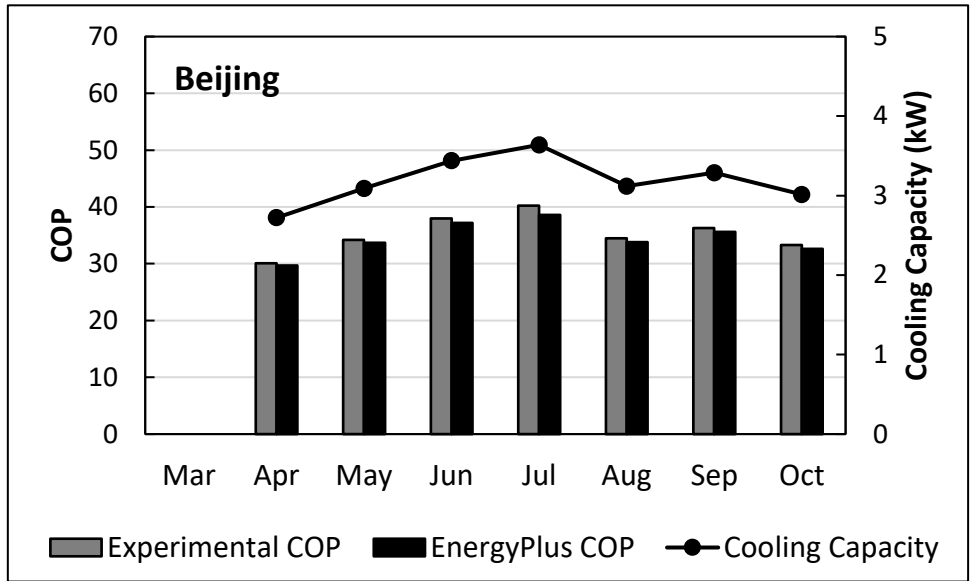
478 Figure 7 presents the comparison of experimental COP and cooling capacity results to
479 EnergyPlus predictions in: (a) Beijing, (b) Rome, (c) Las Vegas, and (d) Riyadh. As seen in
480 Figure 7, the cooling capacity of the actual system and simulations are identical to each
481 other in all the simulated climates. This shows that the calibration of model using the
482 mentioned operational parameters were reflected in the simulation results and the system
483 model is capable of representing actual operation of the DPC. However, other performance
484 parameters (as listed in **Table 4**) need to be checked to ensure that the whole building
485 energy model is also accurate and capable of representing transient interaction of the
486 system with surrounding building.

487 An initial look at the graphs in **Figure 7** reveals that both experimental and simulation values
488 of the COP in all four of the climates follow a similar trend to cooling capacity variations
489 throughout the year. The highest cooling capacity of the system and thus the highest power
490 consumption was observed under hot desert weather conditions of the Riyadh and
491 subtropical hot desert weather conditions of Las Vegas with cooling capacity reaching a
492 peak of 4.6 kW in July.

493 The DPC was required to run for 180 minutes under each weather condition to allow system
494 enough time to stabilize, and the rate of power consumption in Beijing, Rome, Las Vegas,
495 and Riyadh as recorded by experiments were 12.77 kW, 10.21 kW, 13.56 kW, and 15.33
496 kW, respectively. In this study, the rate of power consumption by DPC under different
497 weather conditions is considered instead of the amount of used electricity as the comparison
498 factor. This is mainly because of different running times of the DPC in various regions and
499 hosting facilities which are highly dependent on the weather conditions and the amount of
500 dissipated heat as well as various operating time of facilities. Hence, the rate of power
501 consumption was chosen as comparison factor in order to eliminate impact of inequivalent
502 operating parameters on system performance. Considering the 24-hour operation of DPC
503 during the operating months (as indicated in **Table 3**), the estimated annual consumption
504 values for Beijing, Rome, Las Vegas and Riyadh become 64.4 MWh, 44.1 MWh, 68.3 MWh,
505 and 88.3 MWh, respectively.

506 In case of COPs, the highest values were recorded both by experiments and simulations in
507 four consecutive months (June-September) of Riyadh, reaching experimental peak of 51.1
508 and simulation peak of 49 in July. The lowest COP values, on the other hand, were observed
509 both experimentally (17.7) and by simulation (17.9) in April of Las Vegas. The COP and
510 cooling capacity values in all the climates show an increasing trend towards warmer months
511 of the year and decreasing trends in relatively cooler months. These trends are well justified,

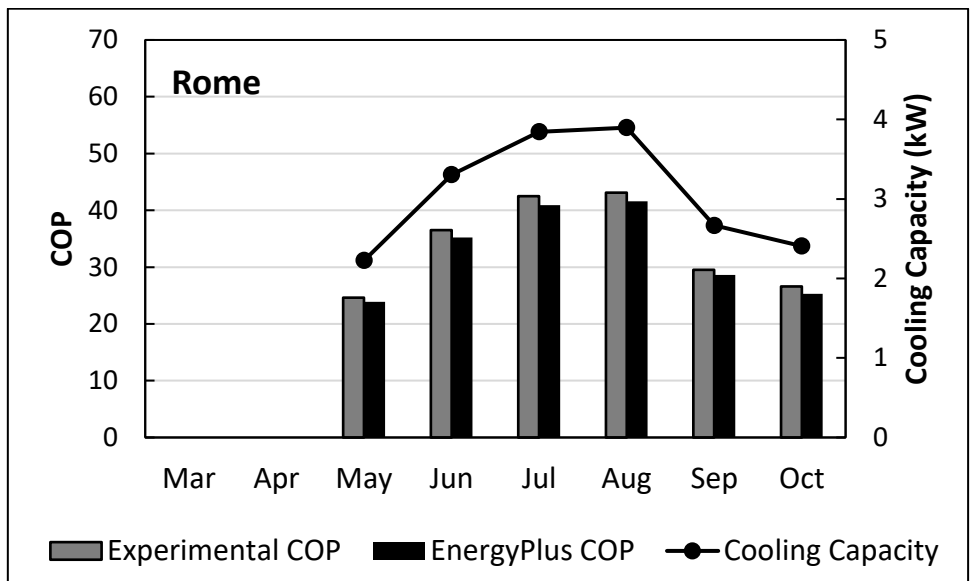
512 considering that both cooling capacity and COP are dependent on external weather
513 conditions (**Equation 1** and **Equation 2**).



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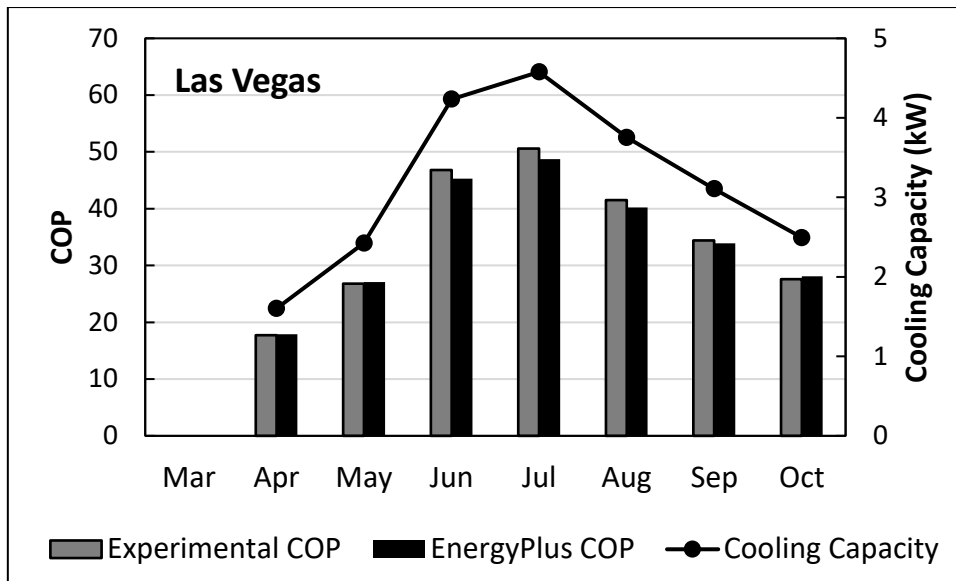
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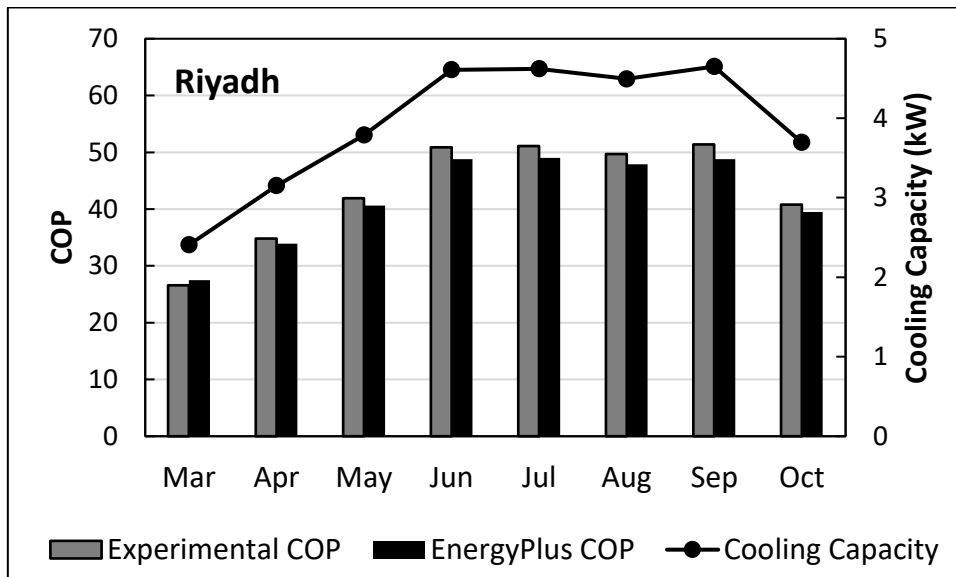
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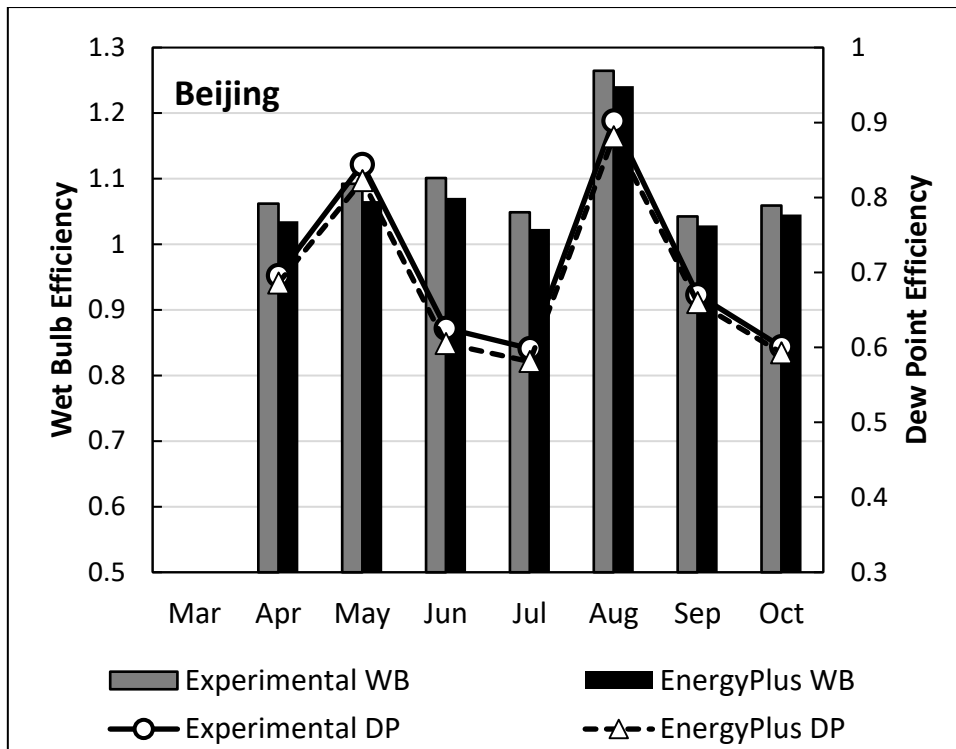
522 **Figure 7** Comparison of experimental COP and cooling capacity results to EnergyPlus
 523 predictions in: (a) Beijing, (b) Rome, (c) Las Vegas, and (d) Riyadh

524 Upon careful calibration of the model, it can be seen in **Figure 7** that experimental COP
 525 results and simulation predictions are in good agreement with a maximum recorded error of
 526 4.13% and mean error of 3.65% in Riyadh, as summarised in **Table 7**. The best fit between
 527 experiments and simulations is achieved in Beijing with mean error of 2.13% followed by Las
 528 Vegas and Rome with mean errors of 2.23% and 3.6%, respectively (**Table 7**). The
 529 simulations predict lower COP values compared to experiment results in majority of the
 530 months, except for April and May in Las Vegas and March in Riyadh where the whole

531 building energy model over-estimated the COP values. This can be related to the sensitivity
532 of model to lower external temperatures and relatively low COP values in these months
533 (<30). With higher COP values, the model tends to predict higher COP values compared to
534 experiment results.

535 **Figure 8** presents the other two performance parameters of the DPC, namely the wet bulb
536 and dew point efficiencies, which are calculated based on inlet and outlet temperatures of
537 the system (**Equation 3** and Equation 4). As can be seen in **Figure 8**, the experimental and
538 simulation values for both wet bulb and dew point efficiencies, in all investigated climates,
539 are in good agreement and are following similar trends throughout the year. A look at the
540 error values in **Table 7** reveals that, similar to COP predictions, EnergyPlus has successfully
541 predicted the efficiencies of the system, presenting a robust case for model validation. The
542 largest monthly difference observed between EnergyPlus and experimental results of the
543 wet bulb and dew point efficiency are 5% (July in Rome) and 4.3% (July in Las Vegas),
544 respectively. Overall, the whole building energy model gave the best predictions of efficiency
545 parameters for Beijing and Las Vegas with mean error values of below 2.5%. The efficiency
546 predictions for Las Vegas and Riyadh, despite being in validation range, showed a larger
547 gap between experimental and simulation results with mean errors of 3.5-3.7%, as seen in
548 **Table 7**.

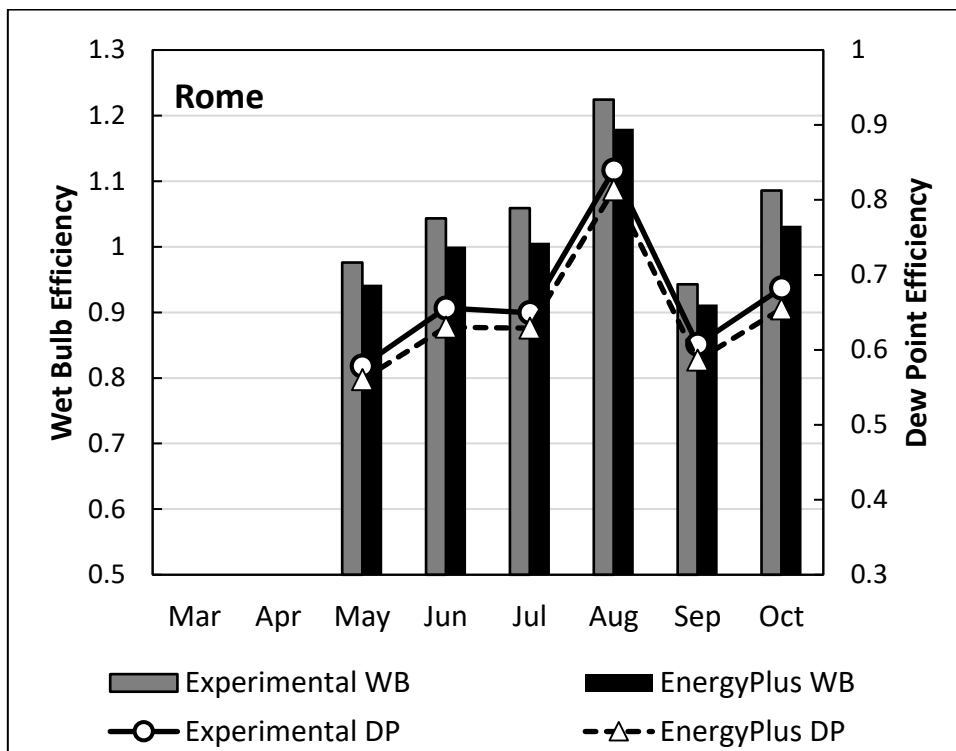
549 The closer investigation of the results in Figure 8, shows that both experimental and
550 simulation results of the efficiency parameters have a steadier rate of variation in Riyadh
551 compared to the other three climates, and hence the DPC performs at a more steady and
552 reliable state. Such stability of operation can be related to two main factors: (i) that the mean
553 monthly external air temperatures, which is fed to the system as working air, has less
554 variations in Riyadh compared to the other investigated climates; and (ii) the Riyadh
555 weather, as a hot desert climate, has the least amount of water content (i.e. humidity)
556 compared to Beijing, Rome and Las Vegas (as seen in **Table 3**). Hence, the statement
557 (supported by both experiments and validated whole building energy model) can be made
558 that the dew point evaporative coolers tend to have more reliable and steady performance in
559 hot desert climates. Such reliable and steady operation of the system, especially in high
560 demand facilities like data centres plays a key role in effective energy management and
561 provides flexibility in dealing with peaks of power consumption. Therefore, it can be
562 concluded that, although higher efficiencies and COP values can be reached in some
563 months of more moderate and humid climates, the sustained and steady operation of the
564 investigated system is achieved in hot and dry climates.



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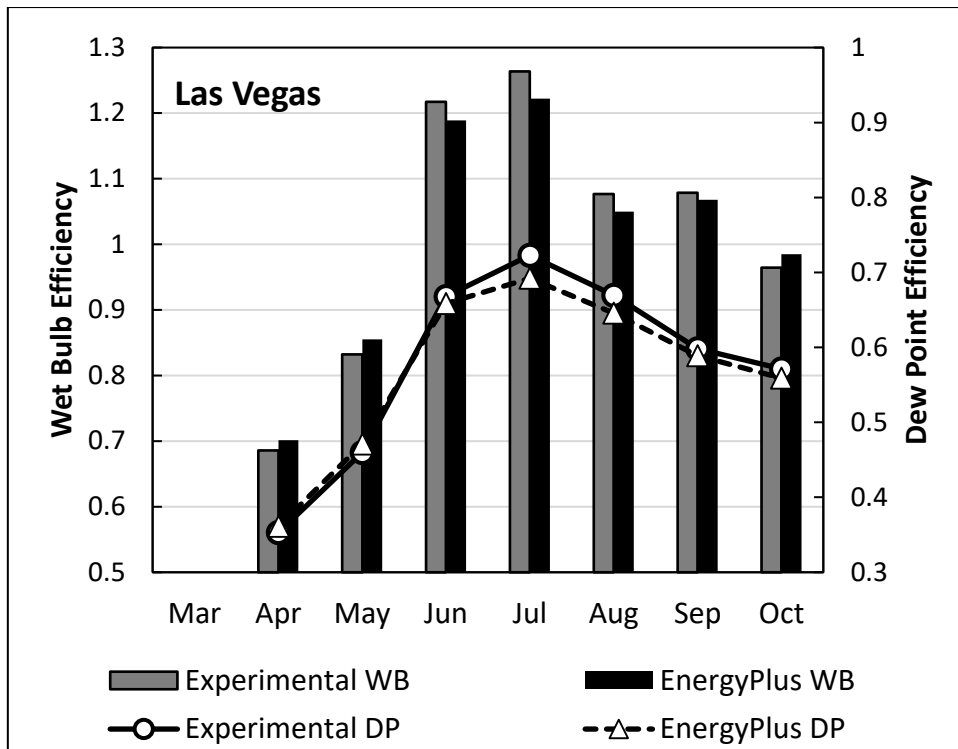
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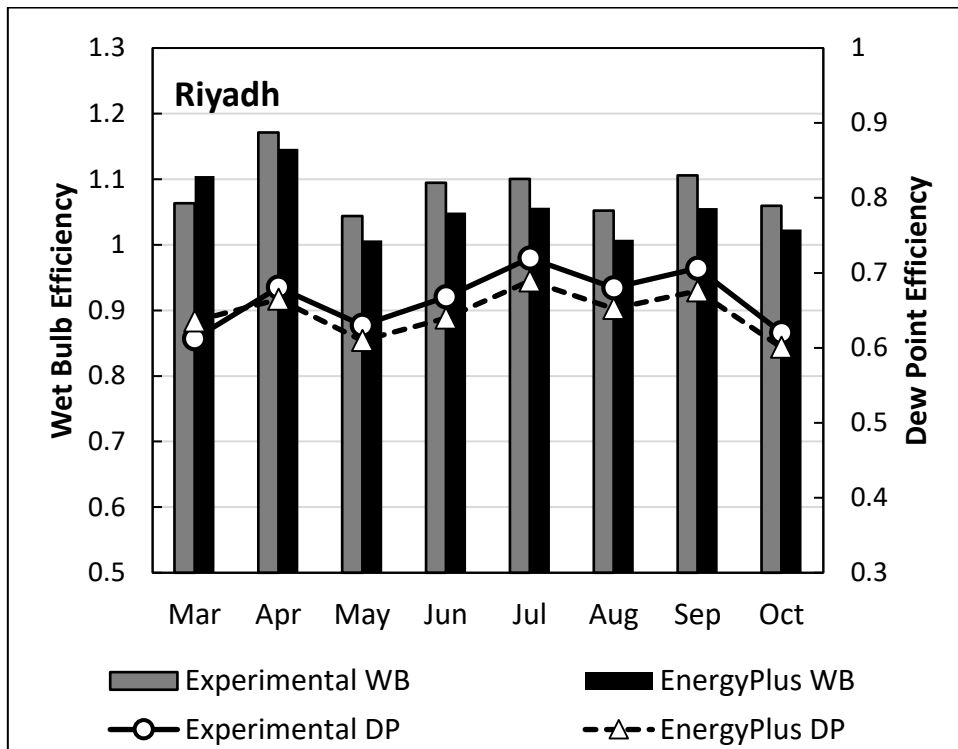
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(c)



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(d)

573 **Figure 8** Comparison of experimental wet bulb and dew point efficiencies to EnergyPlus
 574 predictions in: (a) Beijing, (b) Rome, (c) Las Vegas, and (d) Riyadh

575 **Table 7** Monthly and average difference between experimental values of COP, wet bulb and
 576 dew point efficiencies with EnergyPlus predictions

City	Month	COP Error (%)	Mean COP Error (%)	Wet Bulb Efficiency Error (%)	Mean Wet Bulb Efficiency Error (%)	Dew Point Efficiency Error (%)	Mean Dew-Point Efficiency Error (%)			
Beijing	March	-		-		-				
	April	1.3289		2.5424		1.4799				
	May	1.4620		2.4350		2.5570				
	June	2.1053	2.1337	2.7611	2.0921	3.2614	2.2109			
	July	3.9801		2.4123		2.8911				
	August	2.0290		1.8582		2.3390				
	September	1.9284		1.3427		1.5813				
	October	2.1021		1.2933		1.3643				
March	-			-				-		
April	-			-				-		
May	2.8455			3.4532				3.1460		
Rome	June	3.5616	3.5984	4.1115	4.0664	3.9042	3.4793			
	July	3.7647		4.9679		3.1717				
	August	3.4803		3.6269		3.1201				
	September	3.0509		3.2665		3.4744				
	October	4.8872		4.9724		4.0592				
	March	-				-			-	
	April	-1.1299				-2.3042			-2.3519	
	May	-1.1194				-2.7761			-2.4571	
Las Vegas	June	3.2051	2.2296	2.3334	2.3453	1.3627	2.5300			
	July	3.7549		3.2996		4.2474				
	August	3.1325		2.5258		3.5842				
	September	1.4535		1.0105		1.5714				
	October	-1.8116		-2.1676		2.1351				
	March	-3.3835				-3.9413			-3.8556	
	April	2.5862				2.1431			2.2921	
	May	3.1026				3.5642			3.2688	
Riyadh	June	4.1257	3.6468	4.1301	3.7432	4.2079	3.6714			
	July	4.1096		3.9891		4.2379				
	August	3.6217		4.2391		4.0435				
	September	5.0584		4.5035		4.3053				
	October	3.1863		3.4353		3.1603				

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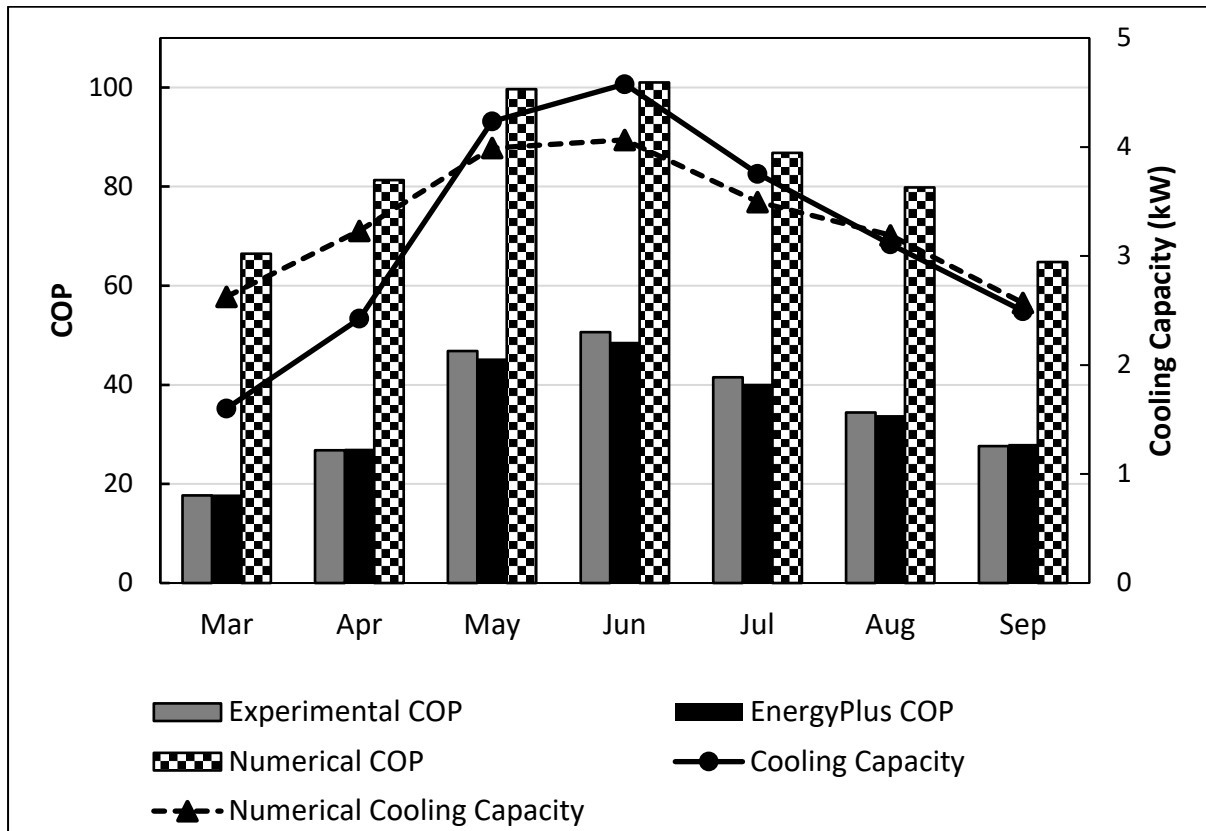
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580 *6.2. Comparison of the whole building energy model results with numerical model:*
581 *superiority analysis*

582 In this section, the whole building energy model is compared to a previously developed
583 numerical model of the same Dew Point Cooler (DPC) [38]. The 8th degree polynomial
584 numerical model (described in **Section 4**) investigated the same cooling system and used
585 the equivalent input parameters as employed by the whole building energy model. Despite
586 the modelling work presented in this study, the numerical model lacks empirical validation
587 and only involves an inter-model comparison to verify the results. Hence, this study offers an
588 unprecedented opportunity to compare performance of a empirically validated whole building
589 energy model, which takes into account the dynamic interaction of the system components
590 with each other and also the interactions of the system with its surrounding building, to a
591 commonly used numerical model; and provide evidence based and critical review of various
592 modelling approaches.

593 The numerical model was developed based on 7857 possible operating conditions, majority
594 of which doesn't happen in real-life operation of the system and only were considered to fully
595 train the model [38]. The performance of the numerical model, after completing the training
596 process was tested in the Las Vegas weather conditions, and hence here only a comparison
597 of experiment results and models' predictions for the city of Las Vegas (Figure 9 and **Figure**
598 **10**) is presented. As can be seen in **Figure 9**, the unrestrained operating conditions
599 employed by the numerical model can lead to COP estimates of up to two times higher than
600 experimental values and EnergyPlus predictions. The numerical model has predicted
601 different cooling capacities compared to the EnergyPlus and the experiments. The main
602 reason for this lies in **Equation 1**, which shows that the cooling load is calculated based on
603 operating parameters (various operating temperatures in this case) which has not be
604 restricted reasonably by the numerical model. Hence, while the matching fan and pump
605 powers are used in both models and the experiments, due to un-restricted operation
606 parameters used by the numerical model, different cooling capacities and consequently
607 different COPs have been predicted by the numerical model. The unrealistic COPs of 100 in
608 June and July as estimated by the numerical model, highlights the critical need for models to
609 take into account the restricting impact of parameters outside system operational conditions,
610 i.e. interaction of the system with hosting building and surrounding environment. The
611 numerical model over-estimates the COP of the system in all of the months that system was
612 operated. The cooling capacity, however, shows a totally biased trend as it is over-estimated
613 by the numerical model in March and April, under-estimated in May, June and July, and
614 closely matches the experimental and EnergyPlus results in August and September (**Figure**
615 **9**).

616 Considering that the COP values are directly co-related to cooling capacity (**Equation 1** and
 617 **Equation 2**), it is expected that the estimates of the two performance parameters by the
 618 numerical model follow a similar trend when compared to experimental and real-life
 619 performance parameters of the system. However, the larger overall difference observed in
 620 COP estimates than the cooling capacity estimates of the numerical model when compared
 621 to experimental values suggests that the numerical model is more sensitive to cooling
 622 capacity variances when it comes to COP calculations.



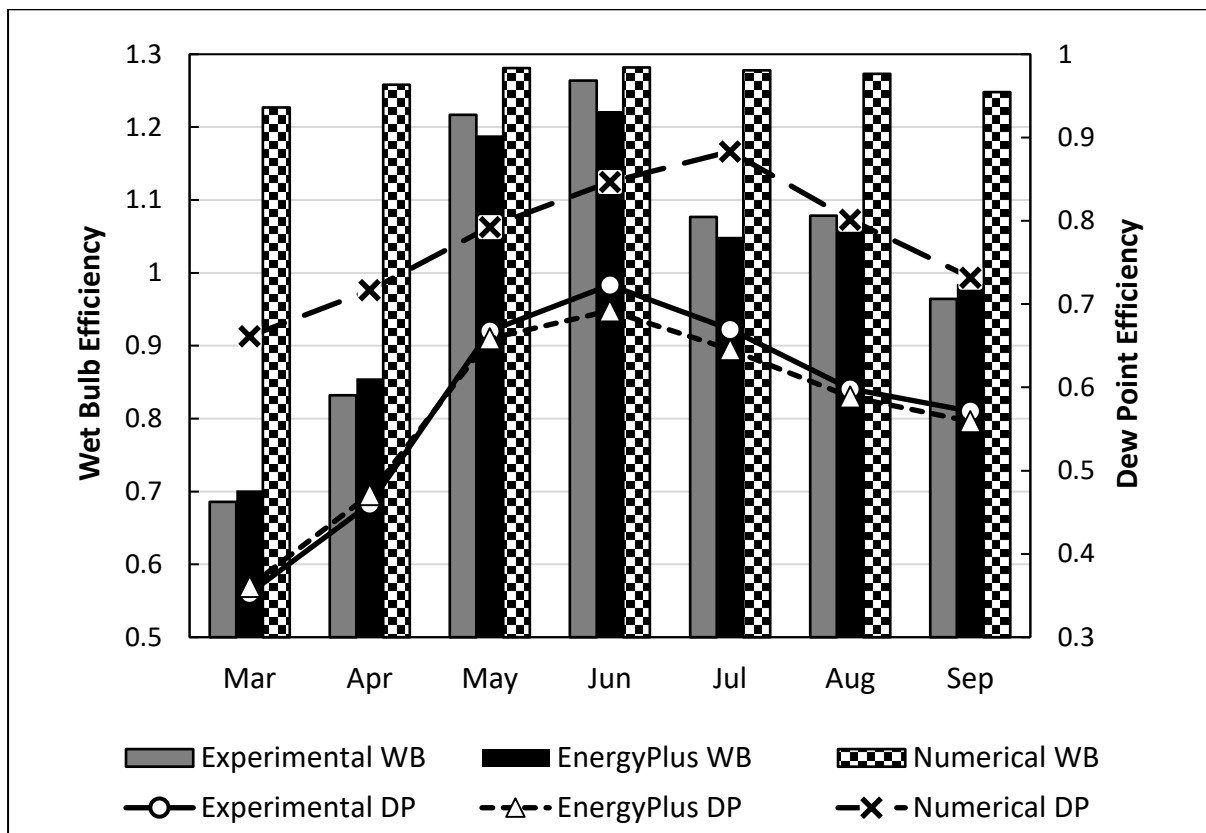
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624 **Figure 9** Comparison of cooling capacity and COP from experiments and EnergyPlus to
 625 numerical model estimates in Las Vegas

626 Investigating the wet bulb and dew point efficiency estimates of the numerical model (**Figure**
 627 **10**) shows that, similar to COP values, the numerical model over-estimates both efficiency
 628 values. The smallest differences between the experimental and numerical model results are
 629 recorded in May and June, and the largest difference in March and April. **Figure 10** clearly
 630 shows that while the validated EnergyPlus model predicts very close efficiencies to the
 631 experiments, the numerical model fails to produce realistic efficiency predictions in most
 632 months. The close agreement of numerical model estimates in May and June shows that the
 633 operating parameters used in these months match with the realistic values, whereas in

634 March and April the trained operating parameters are far from reality, resulting in poor
 635 prediction of the wet bulb and dew point efficiencies.

636 The randomness of the variances in numerical model errors compared to experiments and
 637 EnergyPlus results, as observed in Figure 9 and **Figure 10**, increases the confidence in
 638 concluding that the characteristics difference of the models in simulating operation of the
 639 DPC causes the recorded differences with real life operation of the system. Especially that
 640 the two models (EnergyPlus and numerical) used equivalent and matching input parameters,
 641 proves that the input parameters and unidentified uncertainties didn't have role in poor
 642 performance of the numerical model.



643
 644 **Figure 10** Comparison of wet bulb and dew point efficiencies from experiments and
 645 EnergyPlus to numerical model estimates in Las Vegas

646 Having compared the whole building energy model and numerical model predictions with
 647 each other and with real-life experimental results revealed that despite numerical models'
 648 capacities in swift assessment of evaporative cooling system, these models fail to take into
 649 account the various restraining parameters which would lower the performance parameters
 650 of the investigates system. Hence, the numerical models tend to over-estimate the key
 651 performance parameters like COP, wet bulb and dew point efficiencies resulting in
 652 unrealistic and biased assessment of the system performance. The whole building energy

653 model developed in this study proved to better predict the performance of dew point
654 evaporative cooler by incorporating the building-side parameters into the model and showing
655 very close agreement with experimental performance parameters of the system.

656 Hence, the authors conclude with high certainty that validated whole building energy models
657 can outperform numerical models in assessing performance of dew point evaporative
658 coolers. These models also provide a great opportunity to investigate the system
659 performance in a wide range of hosting buildings, from commercial buildings to schools,
660 hospitals and office buildings, providing valuable insight into the necessary modification that
661 might be necessary before operating the system in various buildings.

662 **7. Conclusion**

663 Faced with increasing interest in Indirect Evaporative Coolers (IECs) as a popular low
664 energy cooling solution for high demand facilities, this study performed a modelling and
665 experimental investigation of a state-of-the-art indirect dew point evaporative cooler. The
666 investigated system was a high-performance counter flow Dew Point Cooler (DPC)
667 employing a guideless and corrugated Heat and Mass Exchanger (HMX) as described in
668 **Section 2**. The experiments were run under four different weather conditions: Beijing as
669 humid continental climate, Rome as Mediterranean climate, Las Vegas as subtropical hot
670 desert climate, and Riyadh as hot desert climate investigating four key performance
671 parameters of the DPC: (i) cooling capacity, (ii) Coefficient of Performance (COP), (iii) wet
672 bulb efficiency, and (iv) dew point efficiency (**Section 3**). The numerical model tested against
673 the experiments was an 8th degree Multiple Polynomial Regression (MPR) model employing
674 6561 operational parameters as the training set and 1296 operational parameters as the
675 validation set. The key operational parameters used in the numerical model were intake air
676 temperature, relative humidity, and flow rate as well as Working air to intake air ratio
677 (**Section 4**). The whole building energy model of the system and the hosting building was
678 developed in the EnergyPlus software package which is an internationally known and tested
679 tool for building energy simulation. The model was calibrated and validated empirically using
680 experimental results (**Section 5**). The whole building energy model results were compared
681 to experiments as part of model calibration and validation. The validated model was then
682 compared to the numerical model to investigate superiority of the two approaches in
683 predicting performance of advance dew point evaporative coolers (**Section 6**). The key
684 findings and conclusions of the study can be summarised as:

- 685 • The highest power consumption was observed under hot desert weather conditions of
686 the Riyadh (15.33 kW) and subtropical hot desert weather conditions of Las Vegas
687 (13.56 kW) with cooling capacity reaching a peak of 4.6 kW in July.

- 688 • The highest COP values were recorded both by experiments and whole building energy
689 simulations in four consecutive months (June-September) of Riyadh, reaching
690 experimental peak of 51.1 and simulation peak of 49 in July.
- 691 • The lowest COP values were observed both experimentally (17.7) and by simulation
692 (17.9) in April of Las Vegas.
- 693 • Experimental COP results and whole building energy simulation predictions were in good
694 agreement with a maximum recorded error of 4.13% and mean error of 3.65% in Riyadh.
- 695 • The best COP fit between experiments and whole building energy simulations was
696 achieved in Beijing with mean error of 2.13% followed by Las Vegas and Rome with
697 mean errors of 2.23% and 3.6%, respectively.
- 698 • The largest difference observed between EnergyPlus and experimental results of the wet
699 bulb and dew point efficiency are 5% (July in Rome) and 4.3% (July in Las Vegas),
700 respectively.
- 701 • The whole building energy model gave the best predictions of efficiency parameters for
702 Beijing and Las Vegas with mean error values of below 2.5%. The efficiency predictions
703 for Las Vegas and Riyadh, despite being in validation range, showed a larger gap
704 between experimental and simulation results with mean errors of 3.5-3.7%.
- 705 • The unrestrained operating conditions employed by the numerical model lead to COP
706 estimates of up to two time higher than experimental values and EnergyPlus predictions.
707 The numerical model over-estimates both efficiency values.
- 708 • The whole building energy model proved to better predict the performance of dew point
709 evaporative cooler by incorporating the building-side parameters into the model.

710 This study proved that comprehensive validation of the numerical model (and generally any
711 model) is a crucial part of any modelling exercise in achieving the most reliable predictions.
712 Hence, the future work by authors will focus on developing hybrid numerical models which
713 take into account the building side parameters and use the data from whole building energy
714 models where necessary to develop robust numerical models capable of representing reality
715 with high precision.

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