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Sonochemical oxidation of piroxicam drug: Effect of key operating parameters and degradation pathways

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17 **Abstract**

18 **BACKGROUND:** Piroxicam (PRX) is a non-steroidal anti-inflammatory drug (NSAID)
19 commonly used to relieve pain and swelling of conditions like arthritis. PRX has been extensively
20 detected in seawater, surface, and sewage waters worldwide and therefore its efficient treatment is
21 an issue of emerging concern. In this work, the sonochemical degradation of PRX was
22 investigated.

23 **RESULTS:** All experiments were conducted at constant ultrasound frequency of 20 kHz while the
24 following range of experimental conditions was investigated: initial PRX concentration 320–
25 960µg/L, ultrasound power density 20–60 W/L, temperature 20–60 °C, reaction time up to 60 min.
26 The effect of different water matrices, namely surface water (SW), bottled water (BW), ultrapure
27 water (UPW) and humic acid (HA) aqueous solution on process efficiency was also explored. It
28 was found that PRX degradation reached 96% after only 10 min of treatment at the best conditions
29 (i.e. [PRX]₀=320 mg/L, 20°C, 36 W/L) assayed. Power density could positively affect PRX
30 degradation. Nevertheless, PRX degradation decreased when its initial concentration and the
31 temperature of the bulk liquid was increased. PRX degradation was found to decrease, in different
32 water matrices, in the order: UPW > 5 mg/L HA > BW > 10 mg/L HA > SW. High resolution mass
33 spectrometry analysis revealed that fourteen transformation by-products (TBPs) were formed and
34 subsequently degraded during treatment while the PRX degradation pathways were also
35 elucidated.

36 **CONCLUSION:** At the optimal operating conditions assayed, PRX was efficiently degraded after
37 about 10 min of sonochemical oxidation, thus rendering it a promising technology for the treatment
38 of xenobiotics

39

40 **Keywords:** NSAIDs; wastewater treatment; ultrasound; pharmaceuticals; intermediate products

41 **1. Introduction**

42 Piroxicam (PRX) is a non-steroidal anti-inflammatory drug (NSAID) commonly used to relieve
43 pain and swelling of conditions like arthritis. NSAIDs, including PRX, have been extensively
44 detected in seawater, surface, and sewage waters worldwide,¹⁻³ since these are among the most
45 frequently used drugs (painkillers, antipyretics, treatment of inflammations and prevention of
46 myocardial infarction). The presence of such drugs, even at low concentrations (from ng/L to
47 mg/L), can have a significant impact on the aquatic and terrestrial systems, and therefore this is an
48 issue of emerging concern.⁴

49 Excretion (from human and animal medical care) is the major source of water and soil pollution
50 by drugs. These are excreted as unchanged or metabolites, which after disposal to municipal
51 sewage systems find their way to the environment.³ Wastewater treatment plants (WWTPs) have
52 been mainly designed to remove suspended solids and organic content while their effect on the
53 removal of micropollutants may be, in most cases, negligible.¹ Therefore, when drugs enter
54 conventional biological WWTPs, only a small fraction is removed and residual amounts are
55 released into the terrestrial and aquatic environment, causing major environmental and health
56 concerns. Due to inadequacy of current WWTPs to completely remove such contaminants,
57 additional or alternative processes should be applied to support existing treatment facilities and
58 increase their efficiency.

59 Sonochemical oxidation is an advanced oxidation process (AOP), which has gained considerable
60 attention over the past decades for the treatment of several trace pollutants, including
61 pharmaceutical substances.⁵⁻⁷ Sonochemical oxidation is based on the in situ generation of
62 powerful oxidizing agents, such as the hydroxyl radical. These are formed through the cyclic
63 formation, growth and implosive collapse of bubbles that behave as hot-spot, micro-reactors.^{8,9} At

64 sufficient contact time and proper operating conditions, sonochemical oxidation may mineralize
65 all organic carbon to CO₂, which is the most stable end product of chemical oxidation. The
66 sonochemical degradation of various NSAIDs, such as ibuprofen,^{10,11} naproxen,¹² and
67 diclofenac¹³⁻¹⁶ has been investigated. Nevertheless, to the best of our knowledge, there is no study
68 on the sonochemical degradation of PRX, a commonly used NSAID. In addition, unlike other
69 drugs, the advanced oxidation of PRX has been merely explored. Specifically, there is only one
70 study by Feng et al.,¹⁷ who investigated the degradation of three NSAIDs, including PRX by means
71 of ozone or H₂O₂/O₃ treatment. That study focused on determining the bio-availability of chemical
72 intermediates formed in ozonated water onto a biofilm-supporting granular activated carbon.

73 The purpose of this work is to investigate the sonochemical oxidation of PRX, evaluate the effect
74 of key operating parameters that can determine degradation rates and propose degradation
75 pathways. Therefore, the following parameters, namely initial PRX concentration, power density,
76 reaction time, water matrix, and temperature are studied. Transformation by-products are
77 identified and a potential degradation pathway is proposed.

78

79 **2. Materials and methods**

80 **2.1 Materials**

81 Piroxicam (PRX) (C₁₅H₁₃N₃O₄S, CAS no: 36322-90-4) was supplied by Sigma–Aldrich and used
82 as received. All experiments, unless otherwise stated, were performed in ultrapure water (UPW)
83 with pH = 6.5 taken from a water purification system (EASYpureRF-Barnstead/Thermolyne,
84 USA). Two more water matrices were employed for this study. One was a commercially available
85 bottled water (BW) (pH = 7.5, 0.4 mS/cm conductivity containing 211 mg/L bicarbonate, 10 mg/L

86 chloride, 15 mg/L sulfate, 5 mg/L nitrate and 78 mg/L of various metal ions), and the other was
87 surface water (SW) collected from a stream near the city of Athens, Greece (pH=7.8, 166 mg/L
88 bicarbonate, 11 mg/ chloride, and 51 mg/L sulfate). Humic acid (HA, CAS number 1415-93-6)
89 was purchased from Sigma–Aldrich. Sodium chloride (NaCl, CAS no: 7647-14-5) and sodium
90 bicarbonate (NaHCO₃, CAS no: 144-55-8), used as free radical scavengers, were purchased from
91 Sigma-Aldrich.

92

93 **2.2 Ultrasound irradiation**

94 A Branson 450 horn-type digital sonifier operating at a fixed frequency of 20 kHz and a variable
95 power output up to 450W (nominal) was employed. Sonochemical oxidation took place in a
96 cylindrical, double-walled, Pyrex vessel, which was open to the atmosphere. Ultrasound irradiation
97 was emitted through a 1 cm in diameter titanium tip which was positioned in the middle of the
98 vessel at a distance of 3 cm from the bottom. The working volume was 0.12 L and the actual power
99 density emitted to the bulk solution was determined calorimetrically and it was found to be
100 between 20 and 60 W/L. Temperature was kept at 20 °C, unless otherwise stated, by a temperature
101 control unit. **Most experiments were performed in duplicate and mean values, whose standard**
102 **deviation never exceeded 5%.** Samples of 1.2 mL were periodically taken from the reactor and
103 analyzed as follows.

104

105 **2.3 Chromatographic techniques**

106 High performance liquid chromatography (HPLC: Alliance 2695, Waters) was employed to
107 monitor the concentration of PRX. Separation was achieved on a Kinetex XB-C18 100A column

108 (2.6 μm , 2.1 mm \times 150 mm) and a 0.5 μm inline filter (KrudKatcher Ultra) both purchased from
109 Phenomenex. The mobile phase consisting of 68:32 water:acetonitrile eluted isocratically at 0.35
110 mL/min and 45 $^{\circ}\text{C}$, while the injection volume was 100 μL . Detection was achieved through a
111 photodiode array detector (Waters 2996 PDA detector, detection $\lambda = 350$ nm). The limit of
112 detection was 3.52 $\mu\text{g/L}$, and the limit of quantitation was 11.75 $\mu\text{g/L}$

113 LC-MS/TOF analysis was carried out on a system, consisted of a Dionex UHPLC Ultimate 3000
114 connected to a BRUKER micrOTOF Focus II mass spectrometer. Gradient methods were
115 developed on a Thermo Scientific AcclaimTM RSLC 120 C18 column (protected by a guard from
116 Waters) thermostated at 30 $^{\circ}$ C, using a mixture of water/1mM ammonium formate and methanol
117 as mobile phase at a flow rate of 0.3 mL/min. The elution starts with 1% methanol and
118 progressively increases to 99% (methanol) at 10 min. At 12 min the initial conditions are reached
119 and retained for 3 min (15 min). The micrOTOF Focus II was operated in both ionization modes
120 (positive and negative) as follows: dry gas at 8 L/min, nebulizer press at 2.4 bar, dry heater at 200 $^{\circ}$
121 C, hexapole RF at 100 Vpp and capillary voltage at 4500 V. Accurate mass measurements provided
122 by micrOTOF Focus II mass spectrometer and the interpretation of fragments derived from in
123 source Collision-induced Dissociation (isCID) was used for the structural assignment of
124 transformation by-products (TBPs).

125

126 **3. Results and discussion**

127 **3.1 Effect of initial PRX concentration**

128 The effect of initial PRX concentration, ranging from 320 $\mu\text{g/L}$ to 960 $\mu\text{g/L}$, on its degradation
129 rate was studied. Figure 1 shows PRX degradation as a function of treatment time at 36 W/L power

130 density, and constant temperature of 20 °C. Complete removal is achieved after 25 min of treatment
131 for 640–960 µg/L PRX and this decreases to almost 10 min when initial PRX concentration is 320
132 µg/L. Data of Figure 1 are found to fit well a pseudo first-order reaction, which is in agreement
133 with previous studies on sonochemical degradation of other NSAIDs, such as ibuprofen ¹⁸ and
134 diclofenac ^{14,15,19}. In the inset graph of Figure 1 it is observed that the kinetic rate coefficients, k,
135 decrease when the initial substrate concentration is increased. For example, rate coefficients are
136 0.1459 min⁻¹, 0.1695 min⁻¹ and 0.2098 min⁻¹ when the initial PRX concentration is 960 µg/L, 640
137 µg/L and 320 µg/L, respectively. The fact that rate coefficient changes with varying PRX
138 concentration implies that the reaction is not true first order although data fitting to first-order
139 kinetics equation (i.e. $\ln [PRX]_0/[PRX]=kt$) is good.

140

141 Figure 1.

142

143 **3.2 Effect of power density**

144 Ultrasound power is a key operating parameter that can substantially affect efficiency of
145 sonochemical oxidation. Therefore, different power densities, ranging from 20 to 60 W/L, were
146 applied for the degradation of 640 µg/L PRX and the results are shown in Figure 2. As seen
147 conversion increases with increasing applied power. Not only this but, as shown in the inset graph
148 of Figure 2, a nearly linear increase of PRX degradation with power density is observed.
149 Specifically, reaction rate coefficients are 0.1157 min⁻¹ ($r^2=0.9688$), 0.1695 min⁻¹ ($r^2=0.9868$) and
150 0.1967 min⁻¹ ($r^2=0.9921$) when power density is 20, 36 and 60 W/L, respectively. This increase of
151 PRX degradation can be attributed to the fact that, at higher power levels, the transmittance of

152 ultrasonic energy into the reactor increases. As a result, a larger number of cavitation bubbles are
153 formed and the pulsation and collapse of bubbles occur at a faster rate, thus increasing significantly
154 the concentration of hydroxyl radicals generated, and the subsequent H₂O₂ production in the liquid
155 mixture, leading to enhanced organics degradation rates.²⁰⁻²² Furthermore, an increase in ultrasonic
156 power contributes to higher mixing intensity due to the turbulence and microstreaming which are
157 generated during the cavitational microbubble collapse,²³ which can also contribute to increased
158 PRX degradation rates.

159

160 Figure 2.

161

162 **3.3 Effect of bulk temperature**

163 Experiments were performed at 20 °C, 40 °C and 60 °C in order to study the effect of temperature
164 on the degradation of 320 µg/L PRX at 36 W/L power density. Results in Figure 3 show that an
165 increase in bulk temperature can reduce process efficiency, and therefore total degradation of PRX
166 is achieved after about 10, 20 and 40 min of sonochemical treatment at 20 °C, 40 °C and 60 °C,
167 respectively. Temperature of the bulk liquid can affect several parameters such as the vapor
168 pressure, viscosity, gas solubility and surface tension. Therefore, the negative effect of temperature
169 on PRX degradation may be explained by the following: the increase in temperature increases the
170 vapor pressure of the solvent. Consequently, the cavitation bubbles contain more water vapor.
171 Because of this increased vapor content, the collapse of the cavitation bubbles is less violent, which
172 is known as the ‘cushioning effect’. This causes a reduction in the collapse temperature and thus a
173 reduced production of •OH radicals. In addition to this, increased temperatures are likely to favour

174 degassing of the liquid phase, thus reducing the number of gas nuclei available for bubble
175 formation.^{20,24}

176

177 Figure 3.

178

179 **3.4 Effect of the water matrix**

180 The complexity of the water matrix is another operating parameter that can affect process
181 efficiency. To assess its effect, experiments were conducted in surface water (SW), bottled water
182 (BW), as well as in UPW spiked with humic acid (HA) at two concentrations (5 and 10 mg/L); in
183 all cases, PRX concentration was 320 µg/L and the power density 36 W/L at 20 °C. Results in
184 Figure 4 show that there is a decrease in the degradation rate in the presence of HA, BW and SW
185 compared to that of UPW. This may be attributed to the fact that HA, BW, and SW contain other
186 organic or inorganic substances that can act as hydroxyl radical scavengers and can therefore
187 significantly lower the degradation of the target contaminant²⁵. Specifically, PRX degradation is
188 found to decrease in the order: UPW (0.2098 min⁻¹) > 5 mg/L HA (0.1005 min⁻¹) > BW (0.0819
189 min⁻¹) > 10 mg/L HA (0.0706 min⁻¹) > SW (0.0646 min⁻¹) with numbers in brackets corresponding
190 to kinetic rate coefficient. The lower degradation rates in the presence of HA, a model natural
191 organic matter (NOM), may be due to the much higher concentration of organic carbon in the
192 solution (5–10 mg/L HA versus 320 µg/L PRX), which competes with the substrate for the
193 oxidative species²⁶. Moreover, it is observed that increase of the initial HA concentration, from 5
194 to 10 mg/L, negatively affects PRX degradation, since the amount of the organics competing with
195 PRX is higher at 10 mg/L than at 5 mg/L HA. PRX degradation in SW, which is the most complex

196 matrix studied, since it consists of NOM and several inorganic substances, is found to be lower
197 than in all other water matrices. Therefore, results indicate that when the complexity of the water
198 matrix is increased process efficiency is decreased.

199

200 Figure 4.

201

202 The presence of chlorides and bicarbonates in BW and SW partially impedes degradation since
203 inorganics can scavenge hydroxyl radicals²⁶. This was further demonstrated by performing
204 experiments in UPW spiked with chlorides, in the form of NaCl, and sodium bicarbonate for
205 degrading 320 µg/L PRX at 36 W/L power density and 20 °C. As shown in Figure 5, PRX
206 degradation rate is substantially decreased in the presence of 250-500 mg/L NaCl as well as of 50-
207 250 mg/L BIC. Results from this work are in agreement with previous studies dealing with the
208 sonochemical degradation of drugs. For example, Xiao et al.¹¹ found that in the presence of
209 terephthalate (TA), a typical •OH scavenger and dissolved Suwannee river fulvic acid (SRFA) the
210 degradation rates of ciprofloxacin and ibuprofen are significantly reduced compared to no TA or
211 SRFA present. Moreover, Gao et al.²² reported that sulfamethoxazole degradation was inhibited
212 in the presence of NO_3^{-1} , Cl^- and SO_4^{-2} and the inhibition degree followed the order of NO_3^{-1} , Cl^-
213 $> \text{SO}_4^{-2}$.

214

215 Figure 5.

216

217 **3.5 Identification of transformation by-products (TBPs) and degradation pathways**

218 Simultaneously with PRX degradation, the formation and subsequent degradation of 14 TBPs was
219 revealed. Structural assignment was based on high resolution accurate mass measurements in both
220 positive and negative ionization mode (Tables 1 and 2). Firstly, under negative ionization mode
221 PRX presents a molecular ion peak $[M-H]^-$ at m/z 330.0554 and fragments (isCID MS) at m/z
222 266.0922 and 210.0224, which correspond to the loss of $-SO_2$ followed intramolecular
223 rearrangement and loss of pyridinecarboxamide moiety, respectively. The fragment ion at m/z
224 146.0602 is generated by the loss of $-SO_2$ followed intramolecular rearrangement from the
225 210.0224 fragment ion. Three TBPs (TBP 9, 10, 12) with molecular ions at m/z 346.0493-
226 346.0506 that differ about 16 amu from the PRX are identified as hydroxylated derivatives.
227 Pyridine, benzothiazine moieties and N-methyl group can be considered as potential sites of
228 hydroxylation. TBP 12 shows a fragment at m/z 226.0180 which corresponds to the loss of
229 pyridinecarboxamide moiety indicating that hydroxylation takes place at the benzothiazine moiety
230 or N-methyl group. On the other hand, TBP 9 and 10 show close retention times but no diagnostic
231 fragments. However, the hydroxylation of PRX molecule in the pyridinyl ring and more
232 specifically at the 5'-position can be proposed for one of the isomeric TBPs since 5'-
233 hydroxypiroxicam is reported as a well-known metabolite of PRX in the literature.²⁸

234 In addition, two di-hydroxylated TBPs (TBP 6 and 11) are detected on the basis of +32 amu
235 difference from the PRX molecule. TBP 11 shows a characteristic diagnostic fragment at m/z
236 210.0224 corresponding to the loss of $C_6H_4N_2O_3$ suggesting that hydroxylation takes place on the
237 pyridinyl ring. Four isomeric TBPs (TBP 4, 5, 7, 8) with m/z 212.0015-212.0030 and TBP 3 are
238 proposed as the mono- and di-hydroxylatedbenzothiazine derivatives, respectively. Finally, TBPs
239 1, 2, 13 and 14 are identified as 1,2-benzisothiazol-3(2H)-one-1,1-dioxide, N-methyl-

240 benzenesulfonamide, N1-(pyridin-2-yl)oxalamide and N1-methyl-N2-(pyridin-2-yl)oxalamide.
241 The profiles (peak area vs irradiation time) of the TBPs are shown in Figure 6. The sequence of
242 the PRX transformation paths can be proposed based on the time within the maximum
243 concentration of each TBP is observed. Therefore, TBPs 9, 10 and 12 (mono-hydroxy-TBPs)
244 peaked up at 120 min allows us to consider them as first-stages TBPs. Di-hydroxylated-PRX
245 derivatives (TBPs 6 and 11) and mono-, di-hydroxylated benzothiazine derivatives (TBPs 4, 5, 7
246 and 8) peaked up at 180 min can be considered as secondary products. Finally, TBPs 1, 2, 13 and
247 14 are detected only in samples after 240 min of treatment and at low concentration levels and thus
248 they can be considered as later stage products. For the sake of comparison with other studies
249 dealing with the degradation of PRX, TBP 14 and structurally similar TBPs have been also
250 identified as degradation products of PRX under oxidative and photolytic conditions.²⁹⁻³² In
251 addition, the in vivo formation of the metabolic oxidation product 5-hydroxypiroxicam and at least
252 13 new secondary peaks (without structure identification) after the in vitro study of hydroxyl
253 radical attack of PRX was reported elsewhere.³³

254 Taking into account the identification and structural assignment of the TBPs, as well as their
255 evolution profiles, the sonochemical degradation mechanisms of PRX are proposed in Figure 7.
256 The first steps of degradation start with hydroxyl radical attack on PRX molecule leading to the
257 formation of hydroxylated, di-hydroxylated derivatives. In parallel, apart from the generation and
258 attack of hydroxyl radicals, singlet oxygen (¹O₂) can be also formed in ample amounts ³⁴ during
259 the ultrasound treatment. PRX quenches ¹O₂ with rate constants in the order of 10⁸ M⁻¹ s⁻¹ showing
260 a significant photodegradation efficiency, as reported elsewhere.³⁵ This pathway proceeds by the
261 addition of singlet oxygen to the enol double bond and the formation of a dioxetane intermediate.
262 Ring cleavage of this unstable intermediate, leads to its conversion in a carboxylic acid structure,

263 as depicted in Figure 7^{29,30,32}, which is further transformed to later stages TBPs, such as TBP 1, 2,
264 13 and 14. The same degradation mechanism was proposed for the photochemical oxidation of
265 PRX.^{29,30,32}

266

267 **4. Conclusions**

268 The aim of this work was to investigate the sonochemical degradation of piroxicam (PRX), a
269 commonly used non-steroidal anti-inflammatory drug. For this purpose, the effect of key operating
270 parameters was evaluated. The following parameters, namely initial PRX concentration,
271 ultrasound power density, temperature, water matrix, and treatment time were studied.
272 Transformation by-products were identified and a potential degradation pathway was identified.
273 The main findings drawn from this study are summarized below.

- 274 • An increase of power density leads to enhanced PRX degradation rates, since at high power
275 densities the amount of hydroxyl radicals generated and the mixing intensity are increased.
- 276 • Increasing the temperature of the bulk liquid results in a reduction of sonochemical activity
277 and this may be attributed to the ‘cushioning’ phenomenon.
- 278 • Water matrices containing organic and inorganic radical scavengers can have adverse effect
279 on degradation kinetics compared to runs in ultrapure water. Also, when the complexity of
280 the water matrix is increased process efficiency is decreased.
- 281 • Sonochemical degradation starts with hydroxyl radical attacking on PRX molecule leading
282 to the formation of hydroxylated and di-hydroxylated derivatives. At the same time, singlet
283 oxygen is added to the enol double bond, thus leading to the formation of a dioxetane

284 intermediate, which is consequently converted to a carboxylic acid structure and other later
285 stages transformation by-products.

286 In general ultrasound irradiation seems a promising technology with relative high efficiency (i.e
287 removal of hundreds of $\mu\text{g/L}$ in less than few minutes) for the destruction of micro pollutants.
288 Further research is needed with particular emphasis at the scale up of the process in order to study
289 the industrial application of sonochemistry in environmental protection.

290

291

292 **References**

- 293 1. Lolić A, Paíga P, Santos LHMLM, Ramos S, Correia M and Delerue-Matos C, Assessment
294 of non-steroidal anti-inflammatory and analgesic pharmaceuticals in seawaters of North of
295 Portugal: Occurrence and environmental risk. *Sci Total Environ* **508**: 240–250 (2015).
- 296 2. Mainero Rocca L, Gentili A, Caretti F, Curini R and Pérez-Fernández V, Occurrence of
297 non-steroidal anti-inflammatory drugs in surface waters of Central Italy by liquid
298 chromatography–tandem mass spectrometry. *Int J Environ Anal Chem* **95**: 685–697 (2015).
- 299 3. Ziyilan A and Ince NH, The occurrence and fate of anti-inflammatory and analgesic
300 pharmaceuticals in sewage and fresh water: Treatability by conventional and non-
301 conventional processes. *J Hazard Mater* **187**: 24–36 (2011).
- 302 4. Bácsi I, B-Béres V, Kókai Z, Gonda S, Novák Z, Nagy SA and Vasas G, Effects of non-
303 steroidal anti-inflammatory drugs on cyanobacteria and algae in laboratory strains and in
304 natural algal assemblages. *Environ Pollut* **212**: 508–518 (2016).
- 305 5. Tran N, Drogui P and Brar SK, Sonochemical techniques to degrade pharmaceutical organic
306 pollutants. *Environ Chem Lett* **13**: 251–268 (2015).
- 307 6. Tran N, Drogui P and Brar SK, Sonoelectrochemical oxidation of carbamazepine in waters:
308 optimization using response surface methodology. *J Chem Technol Biotechnol* **90**: 921–929
309 (2015).
- 310 7. Ma X, Tang K, Li Q, Song Y, Ni Y and Gao N, Parameters on 17 β -Estradiol degradation
311 by Ultrasound in an aqueous system. *J Chem Technol Biotechnol* **89**: 322–327 (2014).

- 312 8. Darsinou B, Frontistis Z, Antonopoulou M, Konstantinou I and Mantzavinos D, Sono-
313 activated persulfate oxidation of bisphenol A: Kinetics, pathways and the controversial role
314 of temperature. *Chem Eng J* **280**: 623–633 (2015).
- 315 9. Oztekin R and Sponza DT, Treatment of wastewaters from the olive mill industry by
316 sonication. *J Chem Technol Biotechnol* **88**: 212–225 (2013).
- 317 10. Méndez-Arriaga F, Torres-Palma RA, Pétrier C, Esplugas S, Gimenez J and Pulgarin C,
318 Ultrasonic treatment of water contaminated with ibuprofen. *Water Res* **42**: 4243–4248
319 (2008).
- 320 11. Xiao R, He Z, Diaz-Rivera D, Pee GY and Weavers LK, Sonochemical degradation of
321 ciprofloxacin and ibuprofen in the presence of matrix organic compounds. *Ultrason*
322 *Sonochem* **21**: 428–435 (2014).
- 323 12. Im J-K, Heo J, Boateng LK, Her N, Flora JRV, Yoon J, Zoh KD and Yoon Y, Ultrasonic
324 degradation of acetaminophen and naproxen in the presence of single-walled carbon
325 nanotubes. *J Hazard Mater* **254**: 284–292 (2013).
- 326 13. Ziylan A, Koltypin Y, Gedanken A and Ince NH, More on sonolytic and sonocatalytic
327 decomposition of Diclofenac using zero-valent iron. *Ultrason Sonochem* **20**: 580–586
328 (2013).
- 329 14. Güyer GT and Ince NH, Degradation of diclofenac in water by homogeneous and
330 heterogeneous sonolysis. *Ultrason Sonochem* **18**: 114–119 (2011).

- 331 15. Naddeo V, Landi M, Scannapieco D and Belgiorno V, Sonochemical degradation of twenty-
332 three emerging contaminants in urban wastewater. *Desalin Water Treat* **51**: 6601–6608
333 (2013).
- 334 16. Naddeo V, Belgiorno V, Kassinos D, Mantzavinos D and Meric S, Ultrasonic degradation,
335 mineralization and detoxification of diclofenac in water: Optimization of operating
336 parameters. *Ultrason Sonochem* **17**: 179–185 (2010).
- 337 17. Feng L, Watts MJ, Yeh D, Esposito G and van Hullebusch ED, The Efficacy of Ozone/BAC
338 Treatment on Non-Steroidal Anti-Inflammatory Drug Removal from Drinking Water and
339 Surface Water. *Ozone Sci Eng* **37**: 343–356 (2015).
- 340 18. Madhavan J, Grieser F and Ashokkumar M, Combined advanced oxidation processes for
341 the synergistic degradation of ibuprofen in aqueous environments. *J Hazard Mater* **178**:
342 202–208 (2010).
- 343 19. Madhavan J, Kumar PSS, Anandan S, Zhou M, Grieser F and Ashokkumar M, Ultrasound
344 assisted photocatalytic degradation of diclofenac in an aqueous environment. *Chemosphere*
345 **80**: 747–752 (2010).
- 346 20. Psillakis E, Mantzavinos D and Kalogerakis N, Monitoring the sonochemical degradation
347 of phthalate esters in water using solid-phase microextraction. *Chemosphere* **54**: 849–857
348 (2004).

- 349 21. Torres RA, Pétrier C, Combet E, Carrier M and Pulgarin C, Ultrasonic cavitation applied to
350 the treatment of bisphenol A. Effect of sonochemical parameters and analysis of BPA by-
351 products. *Ultrason Sonochem* **15**: 605–611 (2008).
- 352 22. Gao Y, Gao N, Deng Y, Gu J, Gu Y and Zhang D, Factors affecting sonolytic degradation
353 of sulfamethazine in water. *Ultrason Sonochem* **20**: 1401–1407 (2013).
- 354 23. Mowla A, Mehrvar M and Dhib R, Combination of sonophotolysis and aerobic activated
355 sludge processes for treatment of synthetic pharmaceutical wastewater. *Chem Eng J* **255**:
356 411–423 (2014).
- 357 24. Emery RJ, Papadaki M, Freitas dos Santos LM and Mantzavinos D, Extent of sonochemical
358 degradation and change of toxicity of a pharmaceutical precursor (triphenylphosphine
359 oxide) in water as a function of treatment conditions. *Environ Int* **31**: 207–211 (2005).
- 360 25. Gogate R, Mujumdar S, Pandit A, Sonochemical reactors for waste water treatment:
361 comparison using formic acid degradation as a model reaction *Adv Environ Res* **7**:283-299
362 (2003).
- 363 26. Rayaroth M, Aravind U, Aravindakumar T, Sonochemical degradation of Coomassie
364 Brilliant Blue: Effect of frequency, power density, pH and various additives. *Chemosphere*
365 **119**: 848-855 (2015).
- 366 27. Guzman-Duque F, Petrier C, Pulgarin C, Penueal G, Torres-Palma R, Effects of
367 sonochemical parameters and inorganic ions during the sonochemical degradation of crystal
368 violet in water. *Ultrason Sonochem* **18**:440-446 (2011).

- 369 28. McKinney AR, Suann CJ and Stenhouse AM, The detection of piroxicam, tenoxicam and
370 their metabolites in equine urine by electrospray ionisation ion trap mass spectrometry.
371 *Rapid Commun Mass Spectrom* **18**: 2338–2342 (2004).
- 372 29. Glass BD, Brown ME, Daya S, Worthington MS, Drummond P, Antunes E, Lebeta M,
373 Anoopkumar-Dukie M and Maharaj D, Influence of cyclodextrins on the photostability of
374 selected drug molecules in solution and the solid-state. *Int J Photoenergy* **3**: 205–211
375 (2001).
- 376 30. Modhave DT, Handa T, Shah RP and Singh S, Successful characterization of degradation
377 products of drugs using LC-MS tools: Application to piroxicam and meloxicam. *Anal*
378 *Methods* **3**: 2864 (2011).
- 379 31. Tománková H and Šabartová J, Determination of potential degradation products of
380 piroxicam by HPTLC densitometry and HPLC. *Chromatographia* **28**: 197–202 (1989).
- 381 32. Ilic-Stojanovic S, Nikolic V, Nikolic L, Zdravkovic A, Kapor A, Popsavin M and Petrovic
382 D, The improved photostability of naproxen in the inclusion complex with 2-
383 hydroxypropyl- β -cyclodextrin. *Hem Ind* **69**: 361–370 (2015).
- 384 33. Gaudiano M., Valvo L, Bertocchi P and Manna L, RP-HPLC study of the degradation of
385 diclofenac and piroxicam in the presence of hydroxyl radicals. *J Pharm Biomed Anal* **32**:
386 151–158 (2003).

387 34. Matsumura Y, Iwasawa A, Kobayashi T, Kamachi T, Ozawa T and Kohno M, Detection of
388 High-frequency Ultrasound-induced Singlet Oxygen by the ESR Spin-trapping Method
389 *Chem Lett* **42**: 1291–1293 (2013).

390 35. Ferrari G V., Natera J, Paulina Montaña M, Muñoz V, Gutiérrez EL, Massad W, Miskoski
391 S and Garcia NA, Scavenging of photogenerated ROS by Oxicams. Possible biological and
392 environmental implications. *J Photochem Photobiol B Biol* **153**: 233–239 (2015).

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396 **List of Tables**

397 **Table 1.** High resolution accurate LC-MS data for PRX and identified TBPs in negative ionization
398 mode (*TBPs detected also in positive ionization mode).

399 **Table 2.** High resolution accurate LC-MS data for PRX and identified TBPs in positive ionization
400 mode (*TBPs detected also in negative ionization mode).

401

402 **Table 1.**

TBP code	R_t (min)	Deprotonated molecular formula	m/z [M-H]⁻	Δ (ppm)	RDBE
TBP1	4.4	C ₇ H ₄ NO ₃ S	181.9925	-4.0	6.5
TBP2	4.7	C ₇ H ₈ NO ₂ S	170.0276	3.2	4.5
TBP3	5.1	C ₈ H ₆ NO ₅ S	227.9972	-1.2	6.5
TBP4	5.4	C ₈ H ₆ NO ₄ S	212.0030	-3.4	6.5
TBP5	6.0	C ₈ H ₆ NO ₄ S	212.0021	0.9	6.5
TBP6*	6.1	C ₁₅ H ₁₂ N ₃ O ₆ S	362.0452	0	11.5
TBP7	6.3	C ₈ H ₆ NO ₄ S	212.0026	-1.2	6.5
TBP8	6.6	C ₈ H ₆ NO ₄ S	212.0015	4.0	6.5
TBP9*	6.9	C ₁₅ H ₁₂ N ₃ O ₅ S	346.0493	3.0	11.5
		C ₁₅ H ₁₂ N ₃ O ₃	282.0875	3.3	11.5
TBP10*	7.1	C ₁₅ H ₁₂ N ₃ O ₅ S	346.0494	2.7	11.5
		C ₁₅ H ₁₂ N ₃ O ₃	282.0875	3.3	11.5
PRX	7.2	C ₁₅ H ₁₂ N ₃ O ₄ S	330.0554	0	11.5
		C ₁₅ H ₁₂ N ₃ O ₂	266.0922	4.9	11.5
		C ₉ H ₈ NO ₃ S	210.0224	2.9	6.5
		C ₉ H ₈ NO	146.0602	6.6	6.5
TBP11*	7.6	C ₁₅ H ₁₂ N ₃ O ₆ S	362.0450	0.7	11.5
		C ₁₅ H ₁₂ N ₃ O ₂	266.0922	4.9	11.5
		C ₉ H ₈ NO ₃ S	210.0224	2.9	6.5
		C ₉ H ₈ NO	146.0602	6.6	6.5
TBP12*	8.0	C ₁₅ H ₁₂ N ₃ O ₅ S	346.0506	-0.8	11.5
		C ₉ H ₈ NO ₄ S	226.0180	-1.4	6.5

403

404 **Table 2.**

TBP code	R_t (min)	Protonated molecular formula	m/z [M+H]⁺	Δ (ppm)	RDBE
TBP13	5.8	C ₇ H ₈ N ₃ O ₂	166.0615	-2.4	5.5
TBP14	6.4	C ₈ H ₁₀ N ₃ O ₂	180.0775	-3.9	5.5
TBP6*	6.1	C ₁₅ H ₁₄ N ₃ O ₆ S	364.0591	1.9	10.5
TBP9*	6.9	C ₁₅ H ₁₄ N ₃ O ₅ S	348.0650	-0.3	10.5
TBP10*	7.1	C ₁₅ H ₁₄ N ₃ O ₅ S	348.0651	-0.7	10.5
PRX	7.2	C ₁₅ H ₁₄ N ₃ O ₄ S	332.0687	3.9	10.5
TBP11*	7.6	C ₁₅ H ₁₄ N ₃ O ₆ S	364.0595	0.8	10.5
TBP12*	8.0	C ₁₅ H ₁₄ N ₃ O ₅ S	348.0650	-0.3	10.5

405

406

407 **List of Figures**

408 **Figure 1.** Effect of initial PRX concentration on its sonochemical degradation at 36 W/L power
409 density with temperature control at 20 °C. Inset graph: Reaction rate coefficient as a function of
410 initial PRX concentration.

411 **Figure 2.** Effect of power density on sonochemical degradation of 640 µg/L PRX with temperature
412 control at 20 °C. Inset graph: Reaction rate coefficient as a function of power density.

413 **Figure 3.** Effect of temperature on sonochemical degradation of 320 µg/L PRX at 36 W/L power
414 density.

415 **Figure 4.** Effect of the water matrix on sonochemical degradation of 320 µg/L PRX
416 sonodegradation at 36 W/L power density with temperature control at 20 °C.

417 **Figure 5.** Effect of (a) NaCl, and (b) bicarbonate (BIC) on the sonochemical degradation of 320
418 µg/L PRX at 36 W/L power density with temperature control at 20 °C.

419 **Figure 6.** Formation and degradation kinetics of identified TBPs under ultrasonic radiation.

420 **Figure 7.** Sonochemical degradation pathways of PRX.

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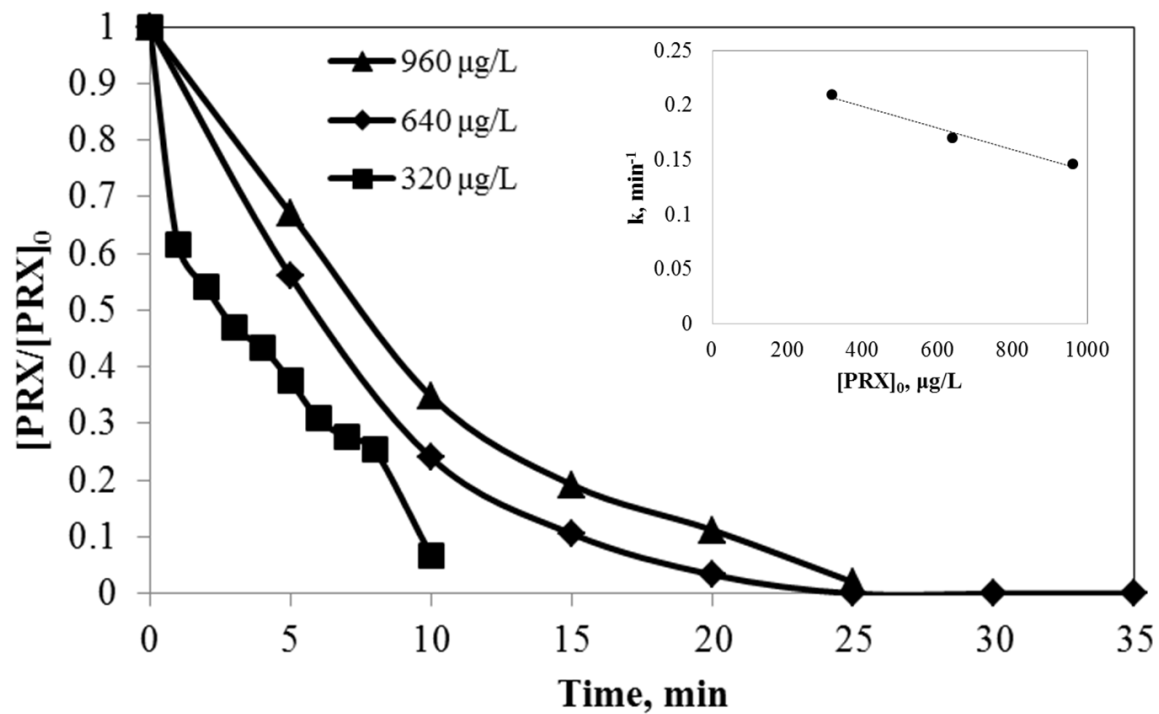
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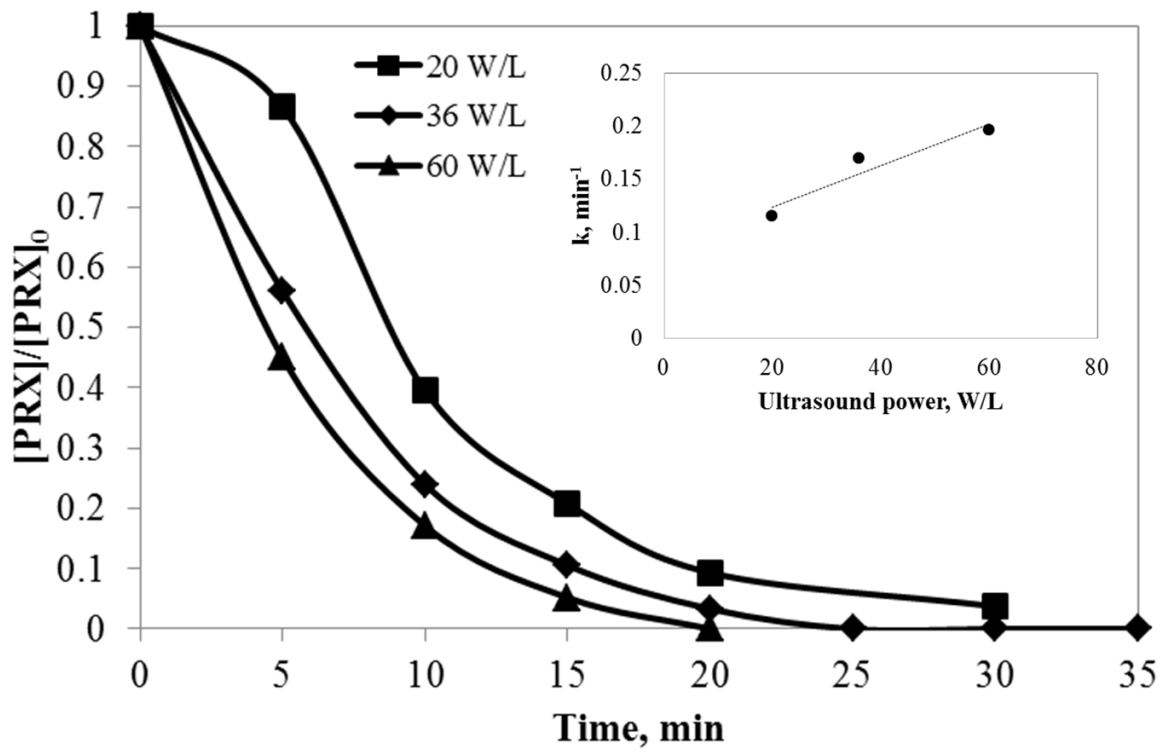
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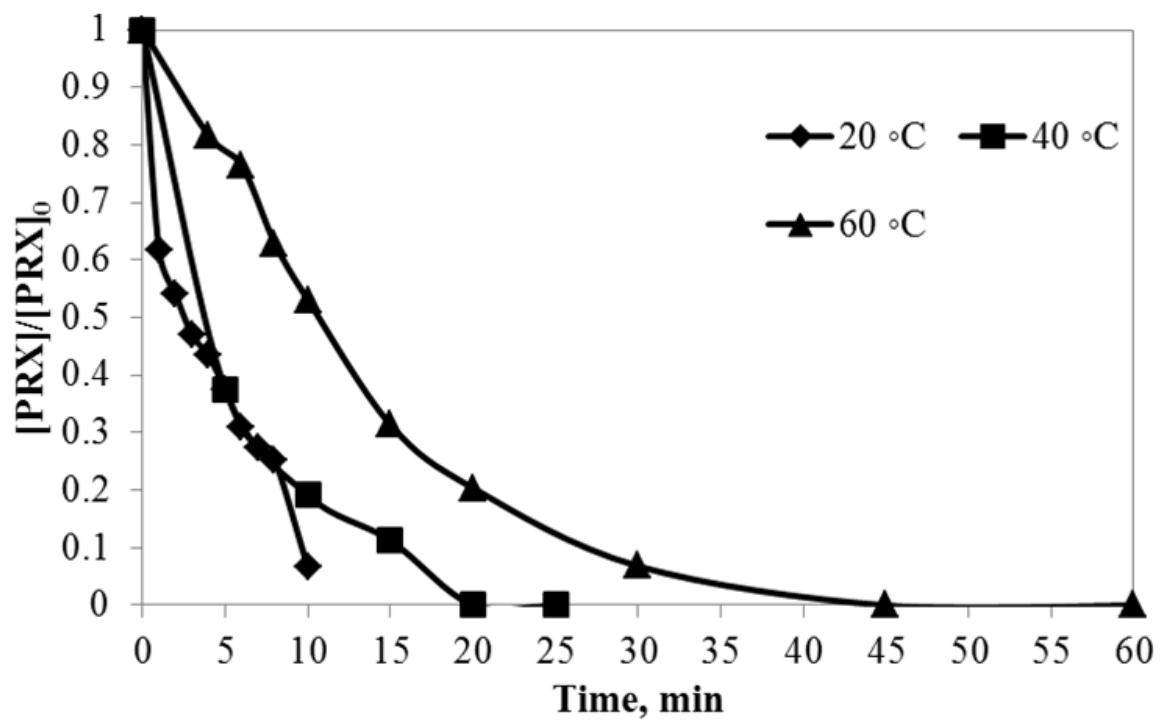


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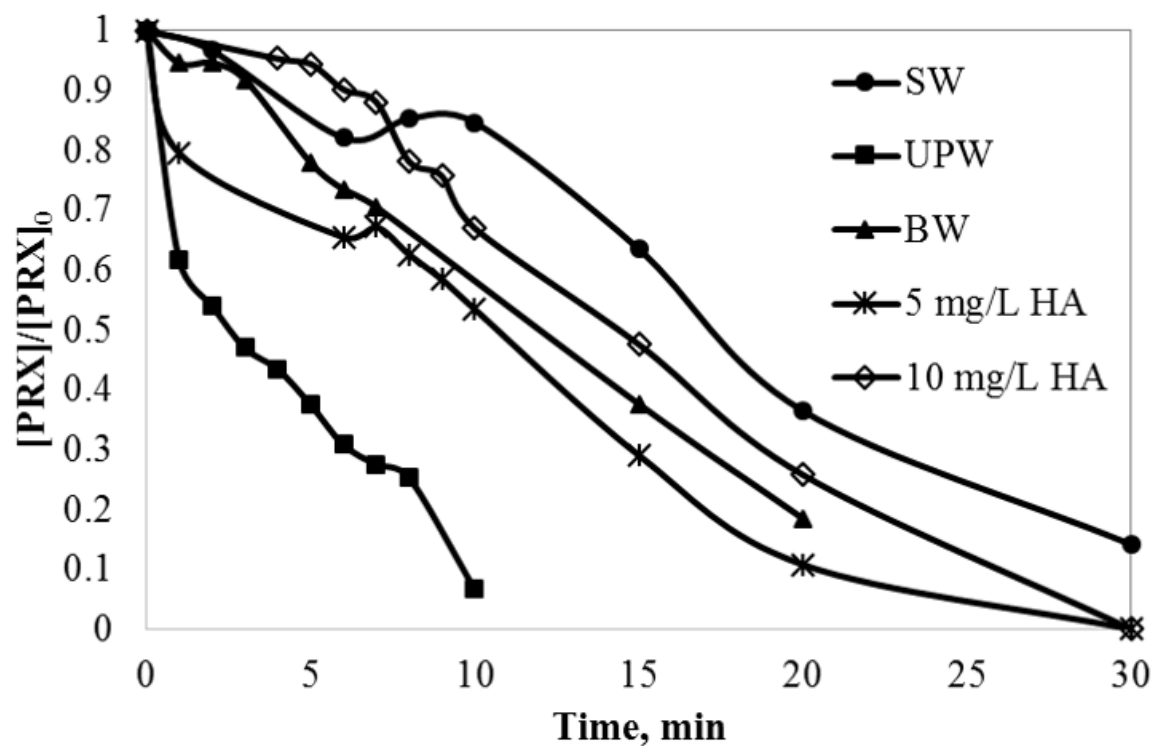
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439 Figure 3

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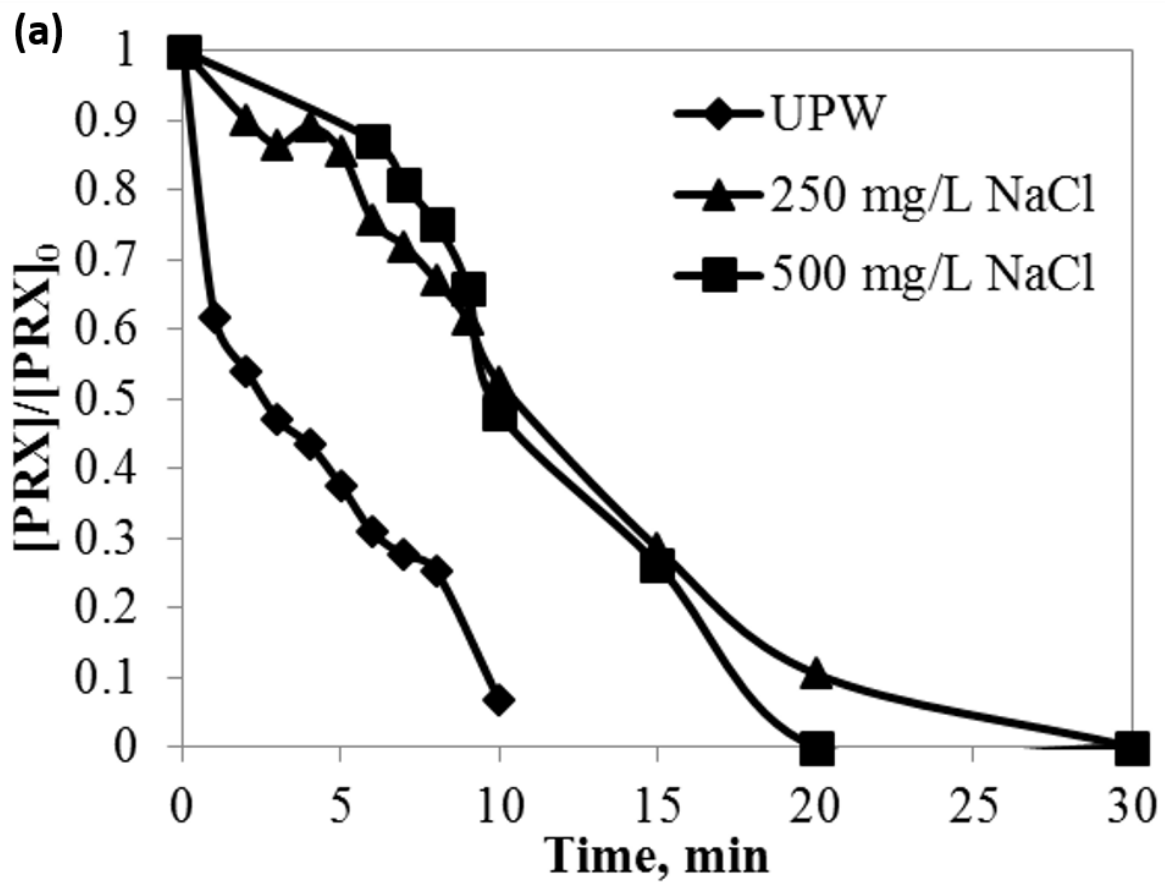
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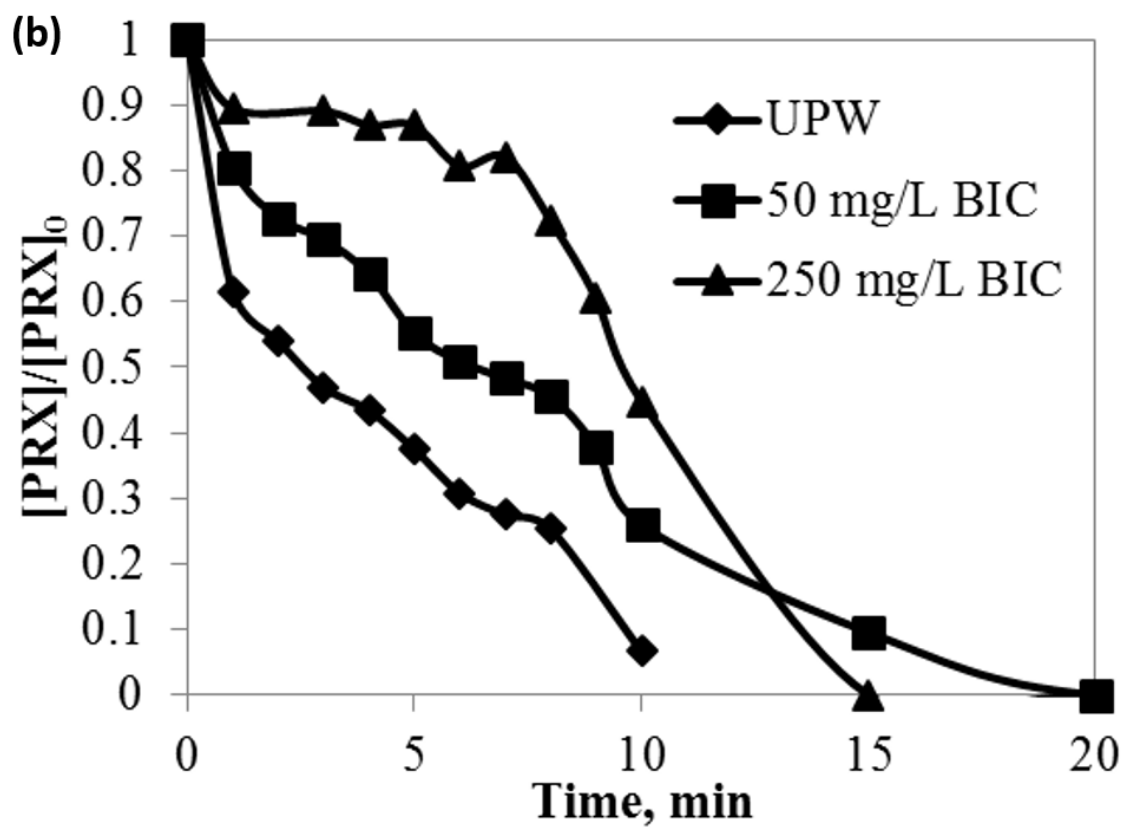
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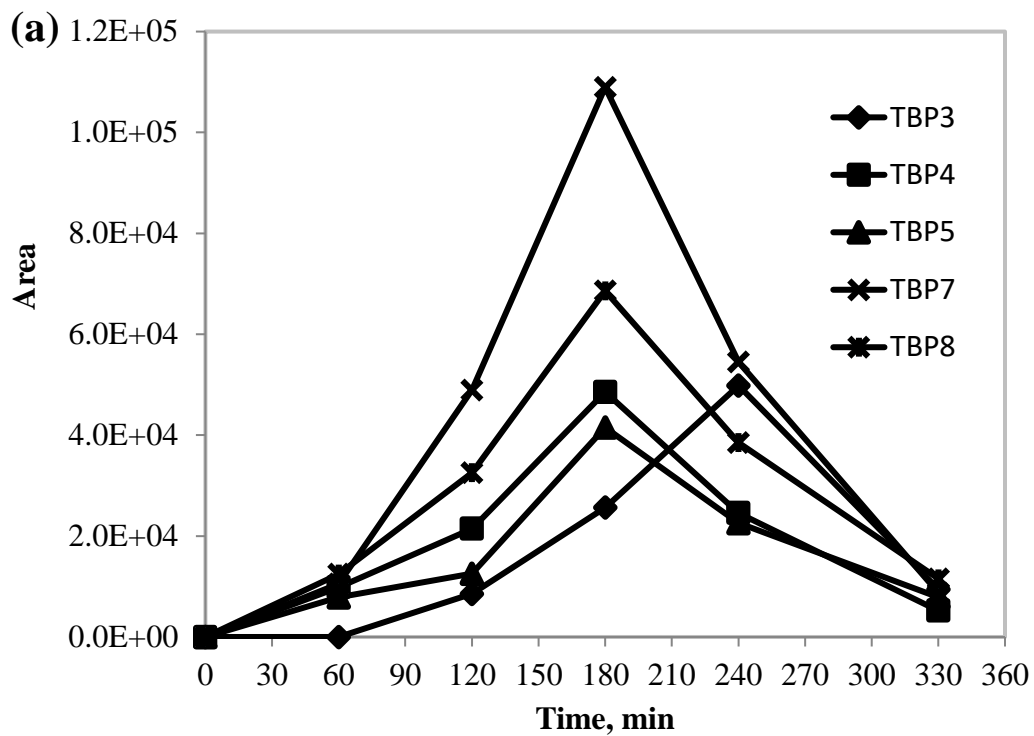
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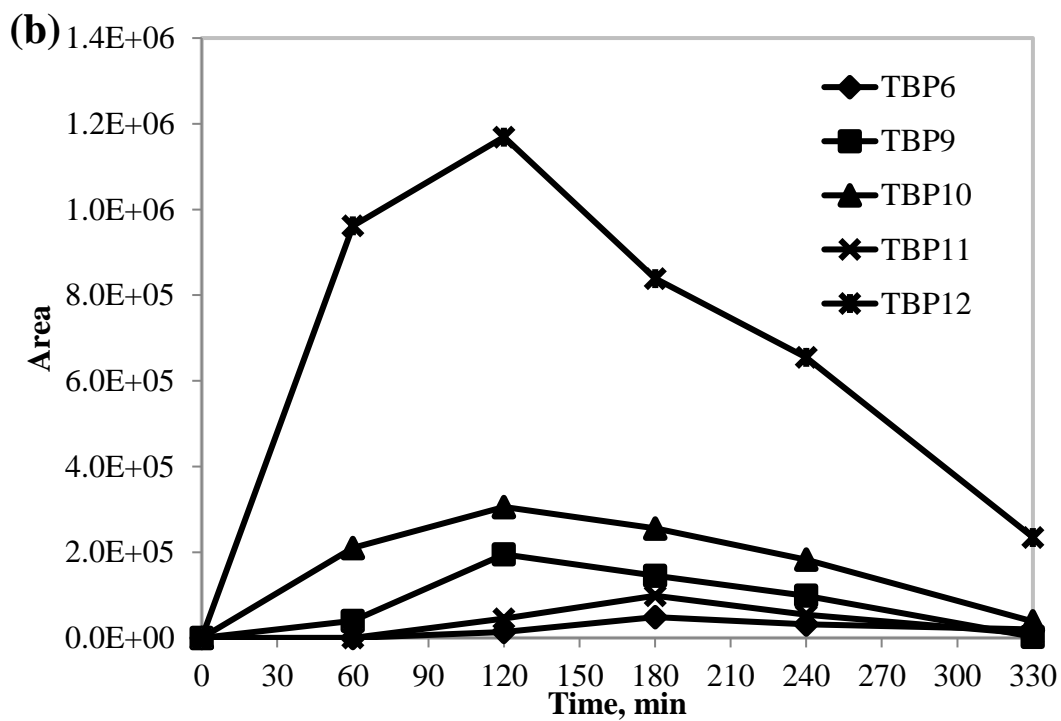
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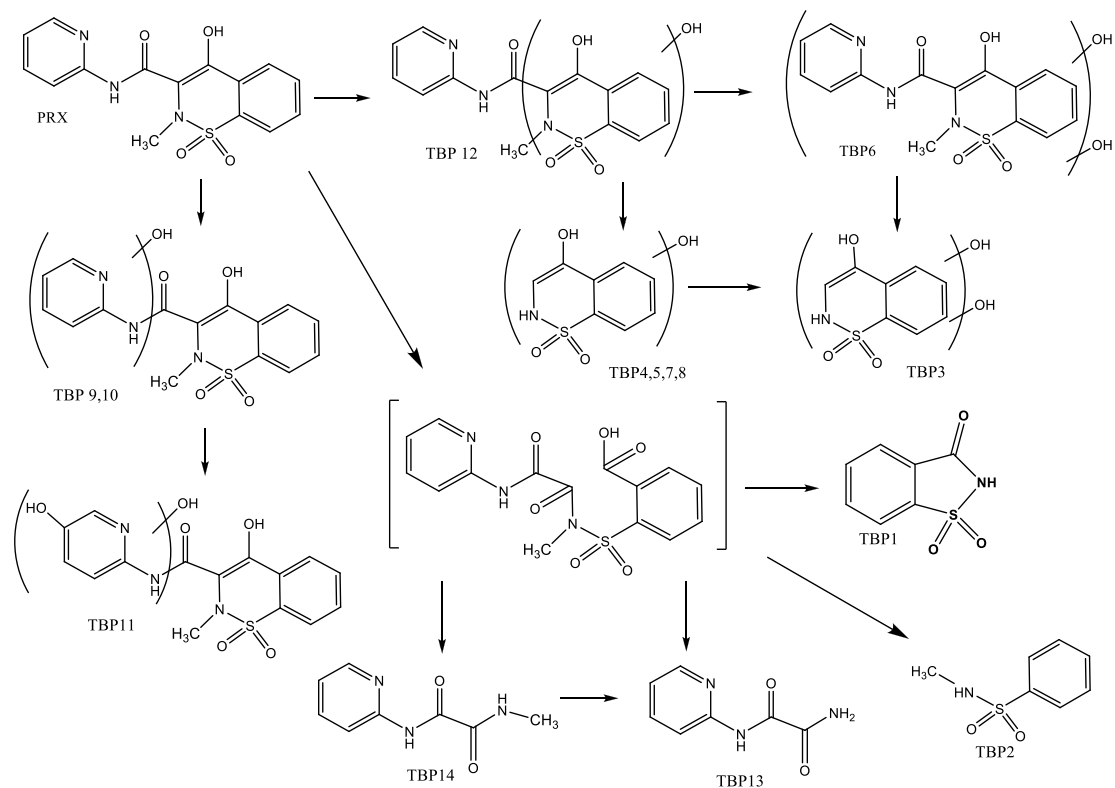


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454 Figure 6

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458 Figure 7

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