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Unsteady Axial Viscoelastic Pipe Flows of an Oldroyd B Fluid

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1. Introduction

The unsteady flow of a fluid in cylindrical pipes of uniform circular cross-section has applications in medicine, chemical and petroleum industries [3,4,5]. For viscoelastic fluids, the unsteady axial decay problem for UCM fluid is considered by Rahman et al. [6]; and for Newtonian fluids as a special case. Rajagopal [7] has studied exact solutions for a class of unsteady unidirectional flows of a second-order fluid under four different flow situations. Atalik et al. [8] furnished a strong numerical evidence that non-linear Poiseuille flow is unstable for UCM, Oldroyd-B and Giesekus models. This fact is supported experimentally by Yesilata, [9]. The unsteady flow of a blood, considered as Oldroyd-B fluid, in tubes of rigid walls under specific APGs is concerned by Pontrelli, [10, 11].

Flow of a polymer solution in a circular tube under a pulsatile APG was investigated by Barnes et al. [12, 13]. The same problem for a White-Metzner fluid is performed by Davies et al. [14] and Phan-Thien [15]. Recently, periodic APG for a second-order fluid has been studied by Hayat et al. [16]. Numerical simulation based on the role of the pulsatile wall shear stress in blood flow, is investigated by Grigioni et al. [1].

The present paper is concerned with the unsteady flow of a viscoelastic Oldroyd-B fluid along the axis of an infinite tube of circular cross-section. The driving force is assumed to be a time-dependent APG in the following three cases:

- i. APG varies exponentially with time,
- ii. Pulsating APG,
- **iii.** A starting flow under a constant APG.

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2. Formulation of the problem

The momentum and continuity equations for an incompressible and homogenous fluid are given by



where ϱ is the material density, *q* is the velocity field, p is the isotropic pressure and <u>S</u> is the Cauchy or extra-stress tensor. The constitutive equation of Oldroyd-B fluid is written as

$$\underline{\underline{T}} = -p\underline{\underline{I}} + S; \underline{\underline{S}} + \lambda_1 \underline{\underline{\underline{S}}} = \mu \{\underline{\underline{A}}_1 + \lambda_2 \underline{\underline{\underline{A}}}_1\}$$
(3)

where <u>T</u> is the total stress, <u>I</u> is the unit tensor, μ is a constant viscosity, λ_1 and λ_2 , $(0 \le \lambda_2 \le \lambda_1)$ are the material time constants, termed as relaxation and retardation times; respectively. The deformation tensor <u>A</u>₁ is defined by

$$\underline{\underline{A}}_{=1} = \underline{\underline{L}} + \underline{\underline{L}}^{T}; \underline{\underline{L}} = \nabla \underline{q}.$$

$$\tag{4}$$

and " ∇ " denotes the upper convected derivative ; i.e. for a symmetric tensor G we get,

$$\stackrel{\nabla}{\underline{G}} = \frac{\partial \underline{G}}{\partial t} + \underline{q} \cdot \nabla \underline{G} - \underline{G} \cdot \underline{L} - \underline{L}^T \cdot \underline{G}.$$
(5)

The symmetry of the problem implies that \underline{S} and \underline{q} depend only on the radial coordinate r in the cylindrical polar coordinates (r, θ ,z) where the z-axis is chosen to coincide with the axis of the cylinder. Moreover, the velocity field is assumed to have only a z-component, i.e.

$$q = (0, 0, \underline{w}), \tag{6}$$

which satisfies the continuity equation (2) identically. The substitution of Eq. (6), into Eqs. (1) and (3) yields the set of equations

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$$S_{rz} + \lambda_1 \frac{\partial S_{rz}}{\partial t} = \mu \left(\frac{\partial w}{\partial r} + \lambda_2 \frac{\partial^2 w}{\partial r \partial t}\right),\tag{7}$$

$$\frac{\partial p}{\partial z} = \frac{\partial S_{rz}}{\partial r} + \frac{1}{r} S_{rz} - \rho \frac{\partial w}{\partial t},$$
(8)
$$\frac{\partial p}{\partial r} = \frac{\partial p}{\partial \theta} = 0.$$
(9)

Equations (8) and (9) imply that the pressure function takes the form; p = z f(t) + c, so that

$$\frac{\partial p}{\partial z} = f(t). \tag{10}$$

The elimination of S_{rz} from (7) and (8) shows that velocity field w(r, t) is governed by:

$$\rho(\lambda_1 \frac{\partial^2 w}{\partial t^2} + \frac{\partial w}{\partial t}) - \mu(1 + \lambda_2 \frac{\partial}{\partial t})(\frac{\partial^2 w}{\partial t^2} + \frac{1}{r}\frac{\partial w}{\partial r}) = -(1 + \lambda_1 \frac{\partial}{\partial t})\frac{\partial p}{\partial z}.$$
(11)

The non-slip condition on the wall and the finiteness of w on the axis give

$$w(r,t)|_{r=R} = 0 \text{ and } \frac{\partial w}{\partial r}|_{r=0} = 0.$$
 (12)

Introducing the dimensionless quantities

$$\eta = \frac{r}{R}, \tau = \frac{\mu t}{\rho R^2}, \varphi = \frac{\mu L}{\Delta P R^2} w, \lambda = \frac{\lambda_2}{\lambda_1} \text{ and } H = \frac{\lambda_1 \mu}{\rho R^2} = \frac{We}{\text{Re}},$$
(13)

where R is the radius of the pipe, ΔP a characteristic pressure difference, L is a characteristic length, *We* and Re are the Weissenberg and Reynolds numbers; respectively, into Eqs. (10), (11) and (12) we get

$$H\frac{\partial^{2}\varphi}{\partial\tau^{2}} + \frac{\partial\varphi}{\partial\tau} - [1 + \lambda H\frac{\partial}{\partial\tau}][\frac{\partial^{2}\varphi}{\partial\eta^{2}} + \frac{1}{\eta}\frac{\partial\varphi}{\partial\eta}] = [1 + H\frac{\partial}{\partial\tau}]\Psi(\tau),$$
(14)

with the BCs.

$$\varphi(1,\tau) = 0 \text{ and } \frac{\partial \varphi(0,\tau)}{\partial \eta} = 0,$$
 (15)



Equation (14) subject to BCs. (15) is to be solved for different types of APGs; i.e. different forms of the function $\Psi(\tau)$.

3. Pressure gradient varying exponentially with time

We consider the two cases of exponentially increasing and decreasing with time APGs separately.

3.1. Pressure gradient increasing exponentially with time

Let,



where K and α are constants. The substitution of Eqs. (17) and (18) into Eq. (14) leads to

$$g'' + \frac{1}{\eta}g' - \frac{\alpha^2(H\alpha^2 + 1)}{\lambda H\alpha^2 + 1}g = -K\frac{H\alpha^2 + 1}{\lambda H\alpha^2 + 1},$$
(19)

while the BCs. (15) reduce to

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$$g(1) = 0, g'(0) = 0 \tag{20}$$

A solution of Eq. (19) subject to the BCs. (20) is

$$g(\eta) = \frac{K}{\alpha^2} [1 - \frac{I_0(\beta \eta)}{I_0(\beta)}],$$
 (21)

where $I_0(x)$ is the modified Bessel-functions of zero-order, and

$$\beta^2 = \frac{\alpha^2 (1 + H\alpha^2)}{1 + \lambda H\alpha^2} \quad . \tag{22}$$

Therefore, the velocity field is given by

$$\varphi(\eta,\tau) = \frac{K}{\alpha^2} \left[1 - \frac{I_0(\beta\eta)}{I_0(\beta)}\right] e^{\alpha^2 \tau}.$$
(23)

The solution given by Eq. (23) processes the following properties:

- i. The time dependence is exponentially increasing such that for $\eta \neq \lim_{\tau \to \infty} \phi(\eta, \tau) \to \infty$. It may be recommendable to choose another APG which increases up to a certain finite limit in order to keep $\phi(\eta, \tau)$ finite.
- **ii.** The present solution depends on the parameter β in the same form as the solution for the UCM [6]. For any value of β the Oldroyd-B fluid exhibits the same form as the UCM- fluid. However, in the present case β depends on λ in addition to H and α^2 . A close inspection show that $\lim_{\lambda \to 0} \beta^2 = \beta^2$ for the UCM-fluid while the $\lim_{\lambda \to 1} \beta^2 = \alpha^2$ which coincides with the case of the Newtonian fluid, [8].
- **iii.** The parameter β is inversely proportional to λ where the decay rate increases by increasing the value of H. However, as mentioned above, as λ approaches the value $\lambda = 1$ all the curves matches together approaching the value $\beta^2 = \alpha^2$ asymptotically. The behavior of β as a function of λ , where H is taken as a parameter is shown in Fig. (1).

For small values of $|\beta|$ and by using the asymptotic expansion of I₀ (x),

it can be shown that the velocity profiles approaches the parabolic distribution;

$$\lim_{\beta \to 0} \varphi(\eta, \tau) = \frac{K(H\alpha^2 + 1)}{4(\lambda H\alpha^2 + 1)} (1 - \eta^2) e^{\alpha^2 \tau}$$
(24)



Figure 1. The $\lambda\beta$ - relation H= 2, 3, 5, 7, 9, (Bottom to top)

For the case of large $|\beta|$ the velocity distribution is given as;

$$\lim_{\beta \to \infty} \varphi(\eta, \tau) = \frac{K}{\alpha^2} \left[1 - \frac{1}{\sqrt{\eta}} e^{-\beta(1-\eta)} \right] e^{\alpha^2 \tau}$$
(25)

This solution is completely different from the parabolic distribution and it depends on η only in the neighborhood of the wall. Therefore, such a fluid exhibits boundary effects.

The rising-APG velocity field $\phi(\eta, \tau)$ is plotted in Figs. (2a) and (2b) as a function of η at different values of β for $\alpha = 2$ and $\alpha = 5$.

3.2. Pressure gradient decreasing exponentially with time

The solution at present is obtained from the previous case by changing α^2 by $-\alpha^{-2}$. Therefore,

$$\varphi(\eta,\tau) = -\frac{K}{\alpha^2} [1 - \frac{j_0(\beta_1 \eta)}{j_0(\beta_1)}] e^{-\alpha^2 \tau}.$$
(26)

where

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Figure 2. Rising – (a,b) APG velocity filed ; β =5.2, 3.5, 2.5, 2.1 (Bottom to top) Fig. (c) : Decreasing – APG velocity filed ; β =8.7, 3.9, 2.6, 2.1 (Top to Bottom) Fig. (d) : Decreasing – APG velocity filed ; β =16.4, 9.2, 6.5, 5.3 (Top to Bottom)

$$\beta_1^2 = \frac{\alpha^2 (1 - H\alpha^2)}{1 - \lambda H\alpha^2} \tag{27}$$

The discussion of this solution is similar to the case of increasing APG except that the velocity decays exponentially with time and the value $\alpha^2 = 1/\lambda H$ is not permissible as it leads to infinite β_1^2 ; i.e. $\lim_{\alpha_1^2 \to 1/\lambda H} \beta_1^2 \to \infty$ (28)

The two cases of small and large $|\beta_1|$ produce similar results as the previous solution. Thus

$$\lim_{\beta_1 \to 0} \phi(\eta, \tau) = -\frac{K}{4\alpha^2} \beta_1^2 (1 - \eta^2) e^{-\alpha \tau} , \qquad (29)$$

and

$$\lim_{\beta_1 \to \infty} \varphi(\eta, \tau) = -\frac{K}{\alpha^2} \left[1 - \frac{1}{\sqrt{\eta}} \frac{\cos(\beta_1 \eta - \frac{\pi}{4})}{\cos(\beta_1 - \frac{\pi}{4})} \right] e^{-\alpha^2 \tau}.$$
(30)

4. Pulsating pressure gradient

The present case requires the solution of Eq. (14) subject to BCs. (15) in the form

$$\Psi(\tau) = -\frac{L}{\Delta P} \frac{\partial p}{\partial z} = K e^{in\tau}; \quad i = \sqrt{-1},$$
(31)

K and n are constants. Assuming the velocity function has the form

$$\varphi(\eta,\tau) = re \left[f(\eta)e^{in\tau} \right], \tag{32}$$

$$\therefore \mathbf{f}'' + \frac{1}{\eta}\mathbf{f}' - in\frac{(1+inH)}{(1+in\lambda H)}\mathbf{f} = -K\frac{(1+inH)}{(1+in\lambda H)}.$$
(33)

The solution of this equation satisfying the BCs. (15) is :

$$f(\eta) = \frac{k}{in} \left[1 - \frac{I_0(\beta\eta)}{I_0(\beta)}\right], \qquad \beta^2 = in \frac{(1+inH)}{(1+in\lambda H)}.$$
(34)

Hence, the velocity distribution is given by:

$$\phi(\eta,\tau) = re\left\{\frac{k}{in}e^{in\tau}\left[1 - \frac{I_0(\beta\eta)}{I_0(\beta)}\right]\right\}.$$
(35)

Obviously; for small $|\beta|$,

$$\lim_{\beta \to 0} f(\eta) = \frac{K}{in} \left(\frac{\beta^2 (1 - \eta^2)}{4} \right).$$
(36)

and for large $|\beta|$

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$$\lim_{\beta \to \infty} \frac{I_0(\beta\eta)}{I_0(\beta)} = \frac{1}{\sqrt{\eta}} e^{-\beta(1-\eta)},\tag{37}$$

So that,

where,
$$\varphi(\eta,\tau) = re\left\{\frac{K}{in}\left[1 - \frac{1}{\sqrt{\eta}}e^{-\beta(1-\eta)}e^{in\tau}\right]\right\},\tag{38}$$

$$\beta^{2} = \frac{in(1+inH)}{(1+in\lambda H)} = \frac{1}{1+n^{2}\lambda^{2}H^{2}} [n^{2}H(\lambda-1) + in(1+n^{2}\lambda H^{2})],$$
(39)

or simply,

$$\beta = \sqrt{\Re} e^{i\theta/2}, \tag{40}$$

$$\Re = \frac{n}{1 + n^2 \lambda^2 H^2} \sqrt{n^2 H^2 (1 - \lambda)^2 + (1 + n^2 \lambda H^2)^2},$$
(41)

$$\frac{\theta}{\lambda} = \frac{1}{2} \operatorname{Tan}^{-1} \left[\frac{1 + n^2 \lambda H}{n H (1 - 1)} \right].$$
(42)

Substituting from Eqs.(40,41,42) into Eq. (37), we get:

$$\lim_{\beta \to \infty} \varphi(\eta, \tau) = \frac{k}{n} \left\{ \sin n\tau - \frac{1}{\sqrt{\eta}} e^{-(1-\eta)\sqrt{\Re}} \cos(\theta/2) \sin[n\tau - (1-\eta\sqrt{\Re}\sin\frac{\theta}{2})] \right\}.$$
(43)
As $\lambda \to 0$, [6], $\Re \to r_1 = n\sqrt{1+n^2H^2}$ and $\frac{\theta}{2} \to \frac{\theta_1}{2} = -\frac{1}{2}Tan^{-1}(\frac{1}{nH}).$

Then

$$\varphi(\eta,\tau) = \frac{k}{n} \left\{ \sin n\tau - \frac{1}{\sqrt{\eta}} e^{-(1-\eta)\sqrt{r_1}(\cos\theta_1/2)} \sin[n\tau - (1-\eta)\sqrt{r_1}(\sin\frac{\theta_1}{2})] \right\}$$
(44)

The velocity field $\varphi(\eta,\tau)$ is plotted in Figs. (3a) and (3b); respectively, against η for different values of β . The two limiting cases for small and large $|\beta|$ are represented in three-dimensional Figs. (4a) and (4b) in order to emphasize the oscillating properties of the solution.



Figure 3. a) : Pulsating – APG ; n=2, H=5, β =3.7, 2.5, 1.8, 1.5 (b) : Pulsating – APG ; n=5, H=5, β =6.8, 4.1, 2.9, 2.4 [Top to Bottom for all]



5. Constant pressure gradient

Here we consider the flow to be initially at rest and then set in motion by a constant ABG "- K". Hence, $\Psi(\tau)$; Eq.(14), subject to BCs. (15) reduces to

$$\frac{L}{\Delta P}\frac{\partial P}{\partial z} = -K.$$
(45)

Therefore, we need to solve the equation

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$$H\frac{\partial^2 \Phi}{\partial \tau^2} + \frac{\partial \Phi}{\partial \tau} - [1 + \lambda H\frac{\partial}{\partial \tau}][\frac{1}{\eta}\frac{\partial \Phi}{\partial \eta} + \frac{\partial^2 \Phi}{\partial \eta^2}] = K, \tag{46}$$

subject to the boundary and initial conditions

$$\phi(1,\tau) = 0$$
, for $\tau \ge 0$,
 $\phi(\eta,0) = 0$, for $0 \le \eta \le 1$ (47)

Equation (46) can be transformed to a homogenous equation by the assumption

$$\Phi(\eta,\tau) = \frac{K}{4}(1-\eta^2) - \psi(\eta,\tau), \tag{48}$$

where $\Psi(\eta, \tau)$ represents the deviation from the steady state solution. Hence,

$$\left[\frac{\partial}{\partial\tau}\left(1+H\frac{\partial}{\partial\tau}\right)-\left(1+\lambda H\frac{\partial}{\partial\tau}\right)\left(\frac{\partial^{2}}{\partial\eta^{2}}+\frac{1}{\eta}\frac{\partial}{\partial\eta}\right)\right]\psi=0,$$
(49)

subject to the boundary and initial conditions

$$\Psi(1,\tau) = 0 \text{ for } \tau \ge 0. \tag{50}$$



Assuming that $\psi(\eta, \tau) = F(\eta) \cdot G(\tau)$, Eq.(49) separates to

$$HG'' + (1 + \lambda H\alpha^2)G' + \alpha^2 G = 0,$$
 (52)

$$F'' + \eta^{-1}(1 + \lambda H\alpha^2)F' + \alpha^2 F = 0.$$
(53)

Equation (52) has the solution,

$$G(\tau) = Ae^{\gamma} 1^{\tau} + Be^{\gamma} 2^{\tau}$$
⁽⁵⁴⁾

where γ_1 and γ_2 are the roots of the Eq.(52). On the other hand, Eq. (53) has the solution



The BCs. (50,51) implies that the constant α_m takes all zeros of the Bessel-function J₀ (α_1 , α_2 ,). Hence,

$$\Psi(\eta,\tau) = \sum_{m=1}^{\infty} J_0(\alpha_m \eta) G(\tau), \tag{57}$$

$$\therefore \Psi(\eta, \tau) = \sum_{m=1}^{\infty} J_0(\alpha_m \eta) (A_m e^{\gamma_{1m}\tau} + B_m e^{\gamma_{2m}\tau}).$$
(58)

The initial condition (50) and BCs. (51) will not be sufficient to evaluate the constants A_m and B_m . Hence, it is required to employ another condition. We assume that $G(\tau)$ is smooth about the value $\tau = 0$ and can be expanded in a power series about $\tau = 0$. Assuming $G(\tau)$ to be linear function of τ in the domain about $\tau = 0$, then $G^{''} = 0$ in Eq. (52). Hence

$$(1 + \lambda H \alpha_m^2) \dot{G}_m(0) + \alpha_m^2 G_m(0) = 0,$$
(59)

$$G_m(\tau) = A_m e^{\gamma_{1m}\tau} + B_m e^{\gamma_{2m}\tau},$$
(60)

From which we obtain

$$A_m[(1 + \lambda H\alpha_m^2)\gamma_{1m} + \alpha_m^2] + B_m[(1 + \lambda H\alpha_m^2)\gamma_{2m} + \alpha_m^2] = 0.$$
(61)

To determine the constants A_m and B_m we firstly satisfy the remaining condition (51). Owing to Eq. (58) and the initial condition, Eq. (51), we notice that,

$$\Psi(\eta, 0) = \sum_{m=1}^{\infty} (A_m + B_m) J_0(\alpha_m \eta) = \frac{K}{4} (1 - \eta^2).$$
(62)
Via the Fourier–Bessel series, Eq. (62) leads to,

$$A_m + B_m = \frac{K}{2J_1^2(\alpha_m)} \int_0^1 \eta (1 - \eta^2) J_0(\alpha_m \eta) d\eta.$$
(63)

Performing this integration we get

$$A_{m} + B_{m} = \frac{2K}{\alpha_{m}^{3} J_{1}(\alpha_{m})} - \frac{K}{\alpha_{m}^{2}} \frac{J_{0}(\alpha_{m})}{J_{1}^{2}(\alpha_{m})}.$$
(64)

From Eqs. (61) and (64) we obtain :

$$A_{m} = \frac{\left[(1 + \lambda H \alpha_{m}^{2})\gamma_{2m} + \alpha_{m}^{2}\right]}{(1 + \lambda H \alpha_{m}^{2})(\gamma_{2m} - \gamma_{1m})} \left[\frac{2K}{\alpha_{m}^{3}J_{1}(\alpha_{m})} - \frac{K}{\alpha_{m}^{2}}\frac{J_{0}(\alpha_{m})}{J_{1}^{2}(\alpha_{m})}\right],$$
(65)

$$B_{m} = \frac{\left[(1 + \lambda H\alpha_{m}^{2})\gamma_{1m} + \alpha_{m}^{2}\right]}{(1 + \lambda H\alpha_{m}^{2})(\gamma_{1m} - \gamma_{2m})} \left[\frac{2K}{\alpha_{m}^{3}J_{1}(\alpha_{m})} - \frac{K}{\alpha_{m}^{2}}\frac{J_{0}(\alpha_{m})}{J_{1}^{2}(\alpha_{m})}\right].$$
(66)

Finally, the velocity field has the series representation

$$\phi(\eta, \tau) = \frac{K}{4} (1 - \eta^2) - \sum_{m=1}^{\infty} \frac{J_0(\alpha_m \eta)}{(1 + \lambda H \alpha_m^2)(\gamma_{2m} - \gamma_{1m})} \left\{ [(1 + \lambda H \alpha_m^2)\gamma_{2m} + \alpha_m^2] e^{\gamma_{1m} \tau} \right\}$$

$$-[(1+\lambda H\alpha_m^2)\gamma_{1m} + \alpha_m^2]e^{\gamma_{2m}\tau}\Big\} [\frac{2K}{\alpha_m^3 J_1(\alpha_m)} - \frac{K}{\alpha_m^2} \frac{J_0(\alpha_m)}{J_1^2(\alpha_m)}].$$
(67)

The constant-APG velocity field $\varphi(\eta, \tau)$ as a function of η shown in Fig. (5).



Figure 5. The velocity distribution for constant – APG taking H=0.2, τ =0.1 where the summation is taken for α_1 =2.4, α_2 =5.8, α_3 =8.4

6. Results and discussion

The behavior of $|\beta|$ as a function of λ where H is taken as a parameter is shown in Fig. (1). The behavior of β is inversely proportional to λ while it is fast-decreasing for higher H-values. For any β -value, the Oldroyd-B fluid exhibits the same form as the UCM-fluid. A close inspection of $\beta^2 = \alpha^2(1+\alpha^2H)/(1+\lambda\alpha^2H)$ shows that UCM-fluid is obtained by $\lim_{\lambda \to 0} \beta^2 = \beta^2$ while $\lim_{\lambda \to 0} \beta^2 = \alpha^2$ leads to the case of Newtonian fluid. For small values of $|\beta|$ as well as $|\beta\eta|$ and by using the asymptotic expansion of $I_0(x)$, it can be shown that the velocity profiles approaches the parabolic distribution.

For decay-APGs, Figs. (2a) and (2b) show that the velocity profiles of Oldroyd-B and UCM fluids are parabolic for small values of $|\beta\eta|$ while for large $|\beta\eta|$ they are completely different from this situation. The solutions depend on η only in the neighboring of the wall. Therefore, such fluids exhibit boundary layer effects [17]].

For pulsating-APG, the velocity distribution is represented in Figs. (3a) and (3b). The smallest value of β in both curves is almost parabolic as shown by Eq. (36) while the largest

value exhibits boundary effect as reviled by Eq.(43). To emphasize the oscillating nature of the solution a three-dimensional diagrams (4a) and (4b) for the smallest and largest values of $|\beta|$ are respectively sketched.

Grigioni, et al [1], studided the behavior of blood as a viscoelastic fluid using the Oldroyd-B model. The results obtained for the velocity distribution stands in agreement with the obtained results in the present work.

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References

- [1] Grigioni, M., Daniele, C., and D' Avenio, G. The Role of Wall Shear Stress in Unsteady Vascular Dynamics, Vol. 7, No.3 Sep. (2002).
- [2] Thurston, G. B., The viscoelasticity of human blood, Biophysical Journal, 12, 1205-1217(1972).
- [3] Perspectives in fluid dynamics, A collective introduction to current research, Edited by: Batchelor, G.K., Moffatt, H.K. and Worster, M.G., Cambridge Univ. Press, (2000).
- [4] Tucker, C. L., Fundamentals of computer modeling for polymer processing, III, HANSER Publishers, Munich (1989).
- [5] Bird, R.B., Curtiss.C.F., Armstrong R.C. and Hassager, O., Dynamics of polymeric liquids, Vol.2, Wiley, New York (1987).
- [6] Rahaman, K. D. and Ramkissoon, H., Unsteady axial viscoelastic pipe flows, J.Non-Newtonian Fluid Mech., 57 (1995) 27.
- [7] Rajagopal, K.R., Int. J. Non-linear Mech. 17 (1982) 369.
- [8] Atalik, K. and R. Keunings, R., J. Non-Newtonian Fluid mech. 102, (2002) 299.
- [9] Yesilata, B, Fluid Dyn. Res. 31, 41 (2002).
- [10] Pontrelli, G., Pulsatile blood flow in a pipe. Computers & Fluids, 27 (1998) 367.
- [11] Pontrelli, G, Blood flow through a circular pipe with an impulsive pressure gradient. Math Models Methods in Appi Sci, 10 (2000) 187

- [12] Bames, H.A., Townsend, P. and Walters, K., Rheol. Acta.10 (1971) 517.
- [13] Bames, H.A., Townsend, P. and Walters, K., 244, Nature (1969) 585.
- [14] Davies, J.M., Bhumiratana, S. and Bird, R.B. J. Non-Newtonian Fluid Mech, 3 (1977/1978) 237.
- [15] Phan-Thien, N. and DudekJ, J.Non-Newtonian Fluid Mech., 11 (1982) 147.
- [16] Hayat, T, Asghar, S. and Siddiqui, A.M., Some unsteady unidirectional flows of a Non -Newtonian fluid, Int. J. Eng. Science, 38 (2000) 337.
- [17] Schlichting, H., Boundary- layer theory, McGraw-Hill, New York, 1968

