Hindawi Publishing Corporation Journal of Nanomaterials Volume 2014, Article ID 864914, 20 pages http://dx.doi.org/10.1155/2014/864914



Review Article

Study of Modern Nano Enhanced Techniques for Removal of Dyes and Metals

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Received 16 February 2014; Revised 25 March 2014; Accepted 26 March 2014; Published 20 May 2014

Academic Editor: Fan Dong

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Industrial effluent often contains the significant amount of hexavalent chromium and synthetic dyes. The discharge of wastewater without proper treatment into water streams consequently enters the soil and disturbs the aquatic and terrestrial life. A range of wastewater treatment technologies have been proposed which can efficiently reduce both Cr(VI) and azo dyes simultaneously to less toxic form such as biodegradation, biosorption, adsorption, bioaccumulation, and nanotechnology. Rate of simultaneous reduction of Cr(VI) and azo dyes can be enhanced by combining different treatment techniques. Utilization of synergistic treatment is receiving much attention due to its enhanced efficiency to remove Cr(VI) and azo dyes simultaneously. This review evaluates the removal methods for simultaneous removal of Cr(VI) and azo dyes by nanomicrobiology, surface engineered nanoparticles, and nanophotocatalyst. Sorption mechanism of biochar for heavy metals and organic contaminants is also discussed. Potential microbial strains capable of simultaneous removal of Cr(VI) and azo dyes have been summarized in some details as well.

1. Introduction

Azo dyes are widely used to dye various materials such as leather, plastics, textiles, food, paper, and cosmetics. Overall production of azo dyes in the world is estimated to be one million tons annually. The use of azo dyes in modern world represents a serious problem worldwide [1, 2]. Azo dyes are synthetic compounds [1]. These azo dyes can be differentiated by the presence of one or more azo groups (-N=N-) as a chromophore which linked different aromatic amines or phenols by a double bond [1, 3]. More than 10–15% of applied dyes are released into wastewater during dying process [4]. As fixation of dyestuff on the substrate is not an efficient process, it varies depending upon the method of fixation or level of affinity resulting in production of color water [5], which reduces water quality [6]. As these azo dyes are water-soluble, dyes such as sulfonated azo dyes finally enter into

the environment when released through wastewater and have many carcinogenic and mutagenic effects on various forms of life [7]. It affects photosynthetic activity of plants by limiting penetration of sunlight [6]. Moreover, toxic effects of dyes result in formation of tumor, cancer, and allergies in human and also inhibit growth of bacteria, protozoans, algae, plants, and different animals [8].

Various technologies have been applied for removal of azo dyes including physical, chemical, and biological methods but microbial degradation of dye is an efficient tool for removing pollution from environment [5]. Other microorganisms like fungi and algae decolorize dye in waste water by adsorption instead of degradation; as a result, dyes remain in the environment. However, bacteria completely degrade dyes under certain conditions [9]. Even bacteria can degrade intermediate byproduct such as aromatic amines by the hydroxylase and oxygenase enzyme [2].

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Textile industry effluents with organic pollution often contain heavy metals as well as free ionic metals or in complex form [10]. In biodegradation process, both microbial biomass and its activity are of prime importance. High concentration of heavy metals like Pb, Cr, Cu, Zn, As, and Cd may have adverse effect on microbial growth and activity [11]. Microbial community composition is sensitive to long term exposure of heavy metals and may affect the decomposition property of microbes [12]. However, toxicity of these metals depends upon their availability or presence in wastewater [13].

Chromium (CrVI) is highly toxic metal that a slight increase in its level results in various environmental and health problems. The United States Environmental Protection Agency (US EPA) has added the Cr⁺⁶ in the list of 17 poisoning elements that are major threat to humans, plants, and microorganisms [14]. Industrial effluents are frequently cocontaminated with chromium ions and azo dyes [2]. Toxicity of chromium depends upon its oxidation state chromium 6 which is carcinogenic and highly toxic to all forms of life and it is more mobile and soluble in water while its reduced form chromium 3 is comparatively less toxic as it is insoluble in water [15]. Microorganisms have ability to protect themselves against toxicity of heavy metals by adopting certain mechanisms such as adsorption, uptake methylation, oxidation, and reduction [16]. But excessive concentrations of these metals may negatively influence the microbial activity and its resistant potential to heavy metals. Bacterial resistance to chromate is associated with plasmid or arises from mutation in chromosomes [17].

Chromium constitutes an integral part of many complex azo dyes which are used for dye fixation in wood leather, silk, and paper dyeing industries [18]. The structure of chromium complexes formed through chemical reaction between ${\rm Cr_2O_3}$ and a variety of azo organic compounds that are very stable and difficult to destroy [19]. Therefore, combining existence of other azo dyes along with chromium is not only adding more contamination in wastewater but also rendering bacterial population.

Shi et al. investigated that Cr and Pb have negative impact on soil microbial activity [20]. The effects of Cr and Pb were determined in terms of ratio of microbial biomass C to soil organic C, basal respiration per unit microbial biomass (qCO $_2$), and the ratio of substrate-response respiration to microbial biomass C (substrate responsive qCO $_2$). The ratio of microbial biomass in Cr contaminated soil was 0.42% and in Pb contaminated soil was 0.36%, while qCO $_2$ and substrate-responsive values were high in Pb as compared to Cr contaminated soil (P < 0.01) which indicates like other heavy metals that Cr also has stress on bacterial biomass.

It was studied that sulphate reducing bacteria (SRB) removed 25–30% of initial dye (reactive black B, Ramzol blue, and reactive red RB) from medium in 72 h in the presence of 50 mg L⁻¹ chromium and approximately 95% of chromium VI removal was achieved at the end of 24 h incubation period. Results showed that decolorized dye amount was increased at increasing dye concentration by SRB but decolorization yield remained constant [21]. Such lower yield of dye decolorization shows that chromium has inhibitory effect on bacterial

efficacy of removing dye. Similarly, Khalid et al. has reported that at 250 mg $\rm L^{-1}$ of chromium only 8% decolorization was obtained after 24 h using $\rm Cr_2(SO_4)_3$ whereas in case of $\rm CrCl_3$ in the same time period at higher concentrations (150–250 mg $\rm L^{-1}$) the decolorization was in the range of 31 to 49% only [22].

Recently, several microorganisms have been found which have enzymatic system for individual or simultaneous removal of azo dyes and hexavalent chromium (Cr VI) [2, 14, 22, 23]. Bacterial strains KI (*Pseudomonas putida*) and SL14 (*Serratiaproteamaculans*) have great potential to reduce simultaneously 93% CrVI and 100% decolorization of reactive black-5 azo dye in 24 h at pH 7.2 and 35°C in a batch culture. Individually, 100% removal of CrVI and reactive black-5 dye was obtained in 12 h by strains KI and SL14 [23].

Biodegradation is an effective cleanup technology used for the removal of organic and inorganic contaminants from soil [24]. Only few aerobic bacterial strains that can utilize azo dyes and heavy metals simultaneously as growth substrates have been isolated. Microbial population proliferates when soil is amended with substances capable of sorption and inactivation of growth inhibiting substances [25].

Biochar has adsorption property which can be produced by thermal degradation of organic materials in the absence of air (pyrolysis). As the pyrolysis temperature increases, the surface area and pH of the char increase. Large surface area and high cation exchange capacity increase the effectiveness of the char to adsorb organic and inorganic contaminants [26]. Biochar increases not only the sorption of toxic organic and inorganic contaminants in soil but also the other processes related to sorption such as leaching, dissipation, and toxicity for plants [27]. Degradation of azo dye and heavy metals can be obtained by adsorption, enzymatic degradation, or combining both treatment processes [28]. Efficiency of simultaneous degradation treatment for azo dyes and hexavalent chromium can be enhanced by combining different treatment technologies.

Microbial nanotechnology that is a newly emerged method to produce a nanoparticulate catalyst involves the precipitation of transition metals such as palladium, gold, and iron on bacterial cell wall, resulting in the formation of bionano-Met, where Met = transition metal catalyst [29]. On the base of catalytic nature, metal nanoparticles have been applied in environmental remediation [30]. For example, several studies have investigated the application of Fe(0) nanoparticles to reduce organic and inorganic pollutants [31].

Precipitation of these nanoparticles on bacterial surface increases their degradation potential for pollutants. On availability of electron donor, these nanoparticles tend to catalyze the reduction of contaminants, so rendering them insoluble [32]. A variety of inorganic pollutants such as carcinogenic hexavalent chromium and hexavalent uranium are soluble in their highly oxidized form and become sparingly soluble on reduction (to trivalent chromium and tetravalent uranium in the above case, resp.). On the other hand, several organic compounds such as organic dyes, fertilizers, pharmaceutical

compounds, and intermediates undergo reductive degradation. In all these cases, the contamination levels in the subsurface environment and their downstream flow can be considerably controlled and managed. In this way, study of various useful cleanup technologies is of major concern.

2. Azo Dyes

2.1. Classification of Azo Dyes. Dyes exhibit considerable structural diversity and can be classified by their chemical structure or their application to the fiber type. Dyes must carry one or more functionalities giving the dye color, called chromophores, as well as an electron withdrawing or donating substituents that cause or intensify the color of the chromophores, called auxochrome. The chromophore group can be a base for dye classification. The most important chromophores are azo (-N=N-), carbonyl (-C=O), methine (-CH=), nitro (-NO2), and quinoid groups. The most important auxochromes are amine (-NH3), carboxyl (-COOH), sulfonate (-SO3H), and hydroxyl (-OH) groups [33]. Based on the origin and complex molecular structure, dyes can be classified into three categories: (1) anionic: acid, direct and reactive dyes; (2) cationic: basic dyes; and (3) nonionic: disperse dyes [34]. Among the various classes of dyes, reactive dyes are one of the prominent and most widely used types of azo dyes and are too difficult to eliminate. They are extensively used in different industries, including rubber, textiles, cosmetics, paper, leather, pharmaceuticals, and food [35–37]. The most common group reactive dyes are azo, anthraquinone, phthalocyanine [38], and reactive group dyes [39, 40]. Most of these dyes are toxic and carcinogenic [41]. Dyes may also be classified according to their solubility into soluble dyes like acid, basic, metal complex, direct, mordant, and reactive dyes or insoluble dyes including sulfur, azoic, vat, and disperse dyes.

Almost 109 kg of dyes is produced annually in the world, of which azo dyes represent about 70% by weight [42]. Because such large quantities of azo dyes are being produced and used daily by leather tanning, textile, paper production, food industry, and so forth, and they are known to transform to carcinogenic aromatic amines in the environment, their incorrect disposal is a major environmental concern and can affect human and animal health [43].

2.2. Reduction of Azo Dyes. The detailed brief method for the reduction of azo dyes is shown in Figure 1.

3. Simultaneous Removal Methods

Physicochemical processes were usually inefficient costly and not feasible to a wide range of dye wastewater [44]. However, biological processes, such as biodegradation, bioaccumulation, and biosorption are more favorable due to cost effectiveness, ability to produce less sludge, and environmental benignity [44–46]. Biosorption and bioaccumulation are the two main technologies in biological process for of dye bearing industrial effluents. They possess good potential to replace conventional methods for the treatment of dyes industry

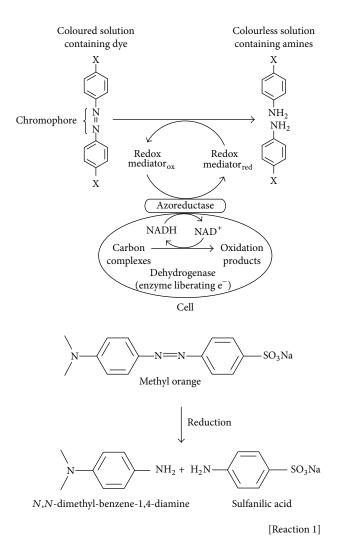


FIGURE 1: Flow sheet diagram for reduction process of azo dyes.

effluents [47]. Biological process can be carried out in situ at the contaminated site; these are usually environmentally benign, that is, no secondary pollution, and they were cost effective. These are the principle advantages of biological technologies for the treatment of dye industry effluents. Hence, in recent years, research attention has been focused greatly on biological methods for the treatment of effluents [36, 48]. The disadvantage of this degradation process is that it suffers from low degradation efficiency or even no degradation for some dyes [1, 5] and practical difficulty in continuous process [36]. Biosorption can be defined as the passive uptake of toxicants by dead or inactive biological materials. The important advantage of biosorption over bioaccumulation process is that the use of living organisms is not advisable for the continuous treatment of highly toxic effluents. This problem can be overcome by the use of dead biomass, which is flexible to environmental conditions and toxicant concentrations.

3.1. Simultaneous Removal by Biochar. Biochar is increasingly receiving attention as a promising functional material in

environmental and agricultural application. It refers to the C-rich residues of incomplete combustion of biomass under oxygen-limited conditions and at relatively low temperatures (<700°C). Various plant tissues and organic-rich wastes including wood chips, animal manure, and crop residues have been used for biochar production. Biochar is produced as a soil amendment for agricultural and environmental gain, which distinguishes it from other carbonaceous products such as activated C (AC) and charcoal [49]. For example, AC is produced from biomass at high temperatures followed by an activation process to increase its surface area for use in industrial processes such as filtration [50].

Extensive work has been done on biochar to slow global warming by sequestering C from atmosphere into soil [33, 49, 51]. Plants absorb atmospheric CO₂ through photosynthesis and store it in their biomass. By heating under oxygen limited condition and at relatively low temperatures, 30-50% C in the biomass is converted to stable biochar, which is primarily composed of condensed aromatic C [49]. Incorporation of biochar into soil has the potential to lock atmospheric C in the solid phase for hundreds to thousands of years [46, 49]. Application of biochar to soil can also help improve soil properties and enhance soil quality by retaining higher moisture and nutrients and microbial activity and therefore increasing crop production [52-54]. Application of biochar to contaminated soils can also reduce the bioavailability of organic contaminants to plants, microbes, and earthworms in contaminated soils [55–57]. The large surface area and high microporosity of biochar are responsible for its high affinity for organic contaminants and large P content is responsible for removal of heavy metals as well (Table 1) [58].

Recently, several studies have been conducted which shows that biochar affects the transport and fate of organic contaminants in soils [55–60]. Hilton and Yuen were the scientists who determined the sorption of pesticide by ashes obtained from burning crop residue even after washing out organic matter with $\rm H_2O_2$ in 1960s [61]. Addition of wheat straw derived biochar to soil effectively sorbed diuron [56]. Yu et al. indicated that the biochar produced from wood chips was effective in immobilizing chlorpyrifos and carbofuran insecticides in a soil [55].

A study conducted by Cao et al. represents that after 210 days of incubation, biochar (P-rich dairy manure) addition reduced atrazine concentration in CaCl₂ extract by 66–81% in both types of soil (Figures 2(a) and 2(b)) [58]. Similarly, atrazine concentrations in the TCLP extract was reduced by 53–77% (Figures 2(c) and 2(d)).

A similar experiment was also performed by application of Pb and biochar in both types of soil. After 120 days of incubation biochar reduced Pb in CaCl₂ extracts by 65–75% in the SR soil and by 57–68% in the BR soil (Figures 3(a) and 3(b)). Similarly, Pb in the TCLP extract was reduced by 72–89% in the SR soil and by 70–79% in the BR soil (Figures 3(c) and 3(d)). Rate of reduction of atrazine and Pb was amplified with increasing biochar level and duration of incubation (Figures 2 and 3).

Mechanism for stabilization of Pb in soil involves the conversion of less stable PbCO₃ into more stable Pb₅(PO₄)₃OH

by P present in biochar, while adsorption of atrazine on organic C in biochar may be responsible for immobilization of atrazine in soil [56].

Phosphorus originally contained in the biochar induced conversion of less stable PbCO₃ to more stable Pb₅(PO₄)₃OH and is responsible for soil Pb immobilization, whereas atrazine stabilization may result from its adsorption on organic C in biochar (Figure 4) [60].

It was investigated by Han et al. that rice straw biochar has great potential to adsorb cadmium (Cd) and sulfamethoxazole (SMX) from cocontaminated water [62]. The calculated maximum adsorption parameter (Q) of Cd was similar in single and binary systems (34129.69 and 35919.54 mg kg⁻, resp.). However, the Q of SMX in a binary system (9182.74 mg kg⁻) was much higher than that in a single system (1827.82 mg kg⁻).

3.1.1. Sorption Mechanism. The good fit of the Langmuir adsorption isotherm was based on monolayer coverage of the adsorbate on the surface of the adsorbent, indicating that the sorption of Cd on rice straw biochar is monolayer sorption on a fixed number of surface sites on the biochar [63]. It was investigated by several experiments that large surface area (SA) is responsible for improving sorption capacity of biochar for heavy metals such as As, Pb, Cu, Zn, and Cd, which provides more surface sites for their adsorption. For example, corn straw char produced at 600°C has a larger SA than hardwood char produced at 450°C, leading to greater adsorption capacities of corn straw char for Cu and Zn [64]. However, in a study conducted by Han et al., different diameters showed no significant effect on the sorption of Cd on biochar, regardless of the presence of SMX (Figure 5) [62]. Xu et al. stated that, in case of adsorbent having low SA (5.61 m² g⁻), sorption may not be influenced by SA of biochar [65]. Therefore, the maximum adsorption capacity of rice straw biochar for Cd calculated by the Langmuir model was similar to the result of the study by Xu et al., which shows that formation of metal-phosphate and carbonate precipitates on the surface of biochar may be attributed to the large adsorption capacity of dairy manure-derived biochar for Cd (32036.85 mg kg⁻) [66]. It was also described by Echeverría et al. that precipitation plays a vital role in the sorption of Cd by adsorbents. In our study, the amount of adsorption was also extraordinarily large [67], and the SEM images (Figure 5) of rice straw biochar after Cd adsorption reveal the precipitates on the surface of the biochar, which confirms that precipitation was responsible for adsorption process.

It was suggested by Harvey et al. that Cd sorption takes place through cation-exchange on biochars produced at $<350^{\circ}$ C, but primarily by two distinctive cation- π bonding mechanisms on biochars produced at $\ge350^{\circ}$ C [68]. Han et al. produced the rice straw biochar at 400° C, which indicates that Cd²⁺- π bonding may contribute to sorption [62]. Sorption of Cd may also be attributed to hydrogenbonding because of the presence of hydroxyl (-OH) in biochar, indicated by the band at 3374 cm⁻¹ [64]. Besides electrostatic interaction, ion exchange could also contribute to Cd sorption on rice straw biochar.

			Maximum ads	orption capacity	Time for max	timum adsorption	
Type of biochar	Organic	Heavy metals	(%)/r	ng kg ⁻	(References	
	compounds		O.C.	Heavy metals	O.C.	Heavy metals	
Rice straw	Sulfamethoxazole (SMX)	Cd(III)	9182.74 mg kg ⁻	35919.54 mg kg ⁻	_	_	[62]
Wheat straw	Diuron	_	_	_	_	_	[56]
P-rich dairy manure	Atrazine	Pb(II)	66-81%	72-89%	210 days	120 days	[58]
Wood chip	Chlorpyrifos and carbofuran insecticides	_	_	_	_	_	[55]
Corn straw	_	Cu(II), Zn(II)	_	_	_	_	[74]

TABLE 1: Adsorption of heavy metals and organic contaminants by biochar.

However, in case of organic contaminant SMX, a positive correlation was found between SA of biochar and the concentration of SMX adsorbed on biochar and the biochar having large diameter (150–250 $\mu \rm m$) was found to attain maximum adsorption capacity for SMX. Scanning electron microscopy (SEM) and the Fourier transform infrared spectroscopy (FTIR) showed that the removal of Cd and SMX by rice straw biochar may be attributed to precipitation and the formation of surface complexes between Cd or SMX and carboxyl or hydroxyl groups.

Because of amino functional groups and N-heteroaromatic rings, SMX is a strong π -acceptor compound [69]. The mechanism of π - π electron donor-acceptor (EDA) [70] facilitates the strong interaction between nitro aromatics and black carbon (char) [71]. In the FTIR spectrum, the π - π EDA interaction between SMX and biochar is because of the COO– groups (1587 cm $^{-1}$) in rice straw biochar.

3.1.2. Effect of pH on Sorption of Heavy Metals. Heavy metal sorption on biochar is positively correlated with pH of medium [62]. Negative charge on the surface of the biochar increases with the increase in solution pH from 3 to 5. Thus, the enhanced electrostatic attraction could promote adsorption of cationic heavy metals on the negatively charged surface of the biochar. There is also competition between protons and metal cations for sorption sites on the surface of the biochar [72].

It was pointed out, in a study conducted by [62], that the amount of Cd adsorption increased with increasing pH and became stable after pH 5 in both single and binary systems. As the pH_{zpc} (zero point of charge) of biochar lies between 2.0 and 3.5 [73], the surface charge of biochar in the solution was mainly negative in the pH range (3, 4, 5, 6, and 7.5) in this experiment. When the pH was above 5, adsorption capacity started decreasing because of the formation of hydroxide complexes [64]. Chen et al. and Liu and Zhang have revealed similar outcomes, regardless of the original material of the biochar [74, 75].

3.1.3. Effect of pH on Sorption of Organic Contaminants. A negative correlation exists between sorption of organic compounds and pH of solution. Increase in pH results in

the reduction of neutral species, whereas anionic species increases, and it creates a strong electrostatic repulsion between the negatively charged biochar surface and organic anionic species. The cationic, neutral, and anionic species of SMX dominate at pH values of <1.7, around 3.7, and >5.7, respectively [76]. This is the most possible reason that the amount of SMX sorption on biochar increased as pH value of solution decreased and it was negatively correlated with the pH values [62].

Moreover, there is strong negative correlation between amount of organic pollutant on biochar and solubility of that contaminant in solution. When pH rises, it may cause less solubility of organic complex and results in reduction of hydrophobic partitioning between organic complex and biochar, supporting that mechanism of hydrophobic partitioning plays a vital role for sorption of organic compounds on biochar. Therefore, sorption of SMX on rice straw biochar decreased on rising pH value (3–7.5) [62]. In addition, by increasing pH value, the π -acceptor ability would increase with protonation, resulting in weaker interaction of π - π EDA between SMX and biochar. This is the one possible reason that sorption level was maximum at pH 3 [62].

3.1.4. Effect of Heavy Metals on Sorption Capacity of Biochar for Organic Contaminants. Earlier studies revealed that either antagonistic [77] or synergistic [78] interaction exists between heavy metals and organic compounds. In the cocontaminated solution, positively charged heavy metals would influence the sorption of organic compounds by altering the biochar surface. Cations could first be adsorbed on the surface of the biochar, and the negative charge on the surface of the biochar would be diminished [79]. Then, the electrostatic repulsion between the biochar surface and anionic organic compounds could be mitigated and therefore significant promotion of adsorption of organic compound. Adsorption of cations (Cd⁺², Ca⁺², Mg⁺², and Cr⁺⁶) could lead to the formation of a bridge on the surface of the biochar [80], assisting the adsorption of organic compound. Deposition of cations on biochar surface could reduce the competition between organic compounds and water for sorption sites by declining the hydrophobicity of the local region [81]. This process not only altered the biochar surface but also formed a

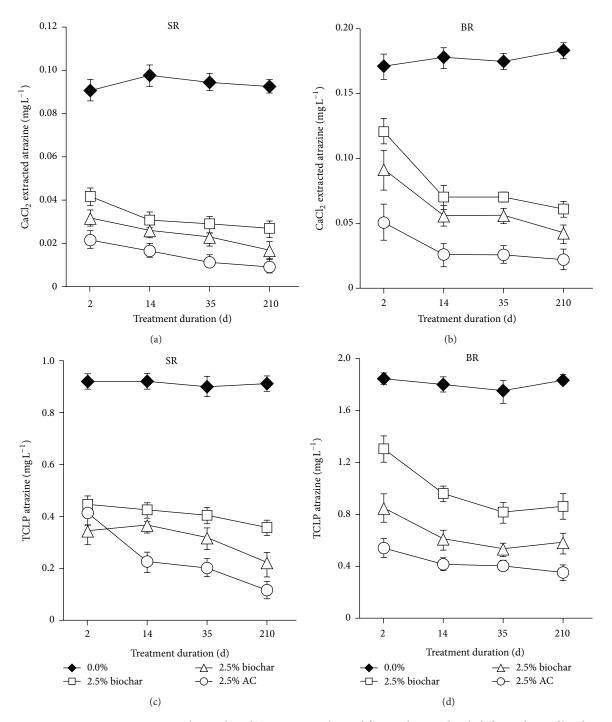
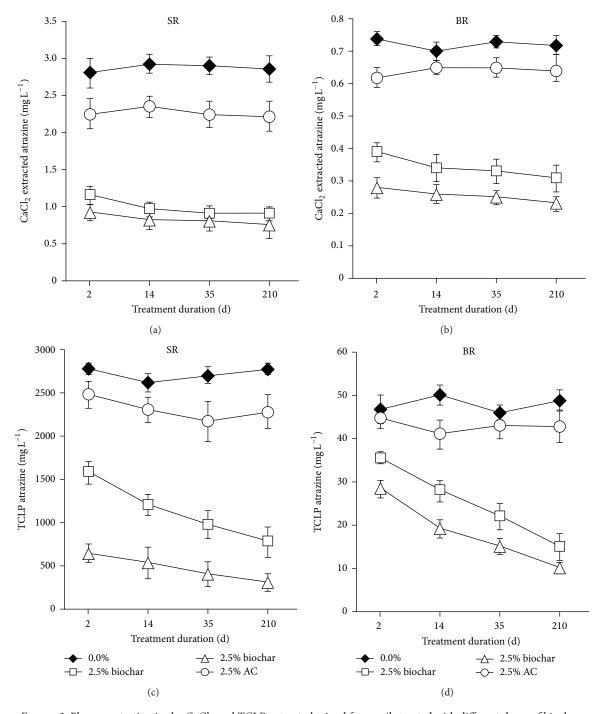


FIGURE 2: Atrazine concentration in the CaCl2 and TCLP extract obtained from soils treated with different doses of biochar.

heavy metal-organic compound complex [82] with a higher sorption affinity on biochar than SMX, based on the metal complexes [83]. A significant increase of SMX sorption on rice straw biochar by Cd was reported by Han et al. (Figure 5) [62].

3.2. Simultaneous Removal by Nanotechnology. In order to solve the problem of water and soil pollution, quick and major

improvements in wastewater treatment have been conducted, comprising photocatalytic oxidation, adsorption/separation processing, and bioremediation; see Table 4 [83]. However, these treatments have been constrained because of many issues such as processing efficiency, operational method, energy requirements, and economic benefit. Currently, nanomaterials (NMs) have been recommended as efficient, costeffective, and environmental friendly substitute to existing



 $FIGURE \ 3: Pb \ concentration \ in \ the \ CaCl_2 \ and \ TCLP \ extract \ obtained \ from \ soils \ treated \ with \ different \ doses \ of \ biochar.$

treatment resources from the perspectives of both resource conservation and environmental remediation [84].

Nanotechnology is a field of applied science, focused on the design, synthesis, characterization, and application of materials and devices on the nanoscale. Nanotechnology holds out the promise of massive progresses in manufacturing technologies, electronics, telecommunications, health, and even environmental remediation [24]. It involves the

manufacture and application of a miscellaneous variety of NMs, which include structures and devices that range in size from 1 to 100 nm and exhibit distinctive characteristics not contained by bulk-sized materials [37]. Various types of nanomaterials exist, such as carbon-based NMs [85], TiO_2NMs [86], and iron oxide NMs [66].

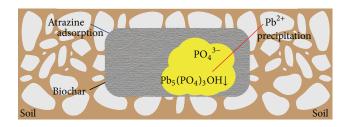


FIGURE 4: Mechanism for Pb(II) precipitation and atrazine adsorption on biochar.

Iron oxides are present in different forms in the universe. Magnetite (Fe₃O₄), maghemite (γ -Fe₂O₃), and hematite (α -Fe₂O₃) are well known. In recent years, the production and utilization of iron oxide NMs with innovative properties and functions have been extensively studied, because of their size in nanorange, high surface area to volume ratios, and superparamagnetism [87]. Predominantly, the easy manufacturing, coating, or amendment and the ability to control or manipulate matter on anatomic scale could offer incomparable flexibility for utilization [88]. Furthermore, iron oxide NMs with low harmfulness, chemical inertness, and biocompatibility represent a remarkable potential coupling with biotechnology because it has great potential to reduce immobilization of microorganisms and in turn provide greater bioavailability of contaminants. In addition, stabilization of nanoparticles on cell surface can improve its stability, reusability, mechanical strength, and the ease of treatment [89].

3.2.1. Simultaneous Removal by Bionanocatalysis. A new biologically inspired method to produce a nanoparticulate catalyst involves the precipitation of transition metals such as palladium, gold, and iron on bacterial surface, resulting in the formation of bionano-Met [29] which have high potential to remove organic and inorganic contaminants from soil and water [90]. Two gram negative model organisms sulfate-reducing bacterium Desulfovibrio desulfuricans [91] and metal-respiring bacterium Shewanella oneidensis [92] have been primarily used to reduce Pd(II) and subsequently induce precipitation of Pd(0) nanoparticles on bacteria and formed the bio-Pd(0) nanoparticles. Ashraf et al. produced a bio-Pd(0) nanocatalyst which successfully reduced the hexavalent chromium (VI) [93].

Recently, Johnson et al. has prepared the bio-Pd(0) nanomaterial by precipitating reduced Pd(0) on *C. pasteurianum* (Figure 6) [29]. Bio-Pd(0) NMs efficiently reduced two azo dyes methyl orange (MO) and Evan's blue (EB). Ten ppm of nano-Pd degraded MO almost 100% in 7 minutes (Figure 7) whereas 5 ppm of bio-Pd(0) decolorized EB almost 100% in 7 minutes (Figure 8).

In another study, it was found that only 50 mg L^- of bio-Pd(0) reduced seven highly toxic PCBs up to 27% of their initial level. Whereas, 500 mg L^- of commercial Pd(0) powder

reduced the same concentration of PCBs [92]. Isolated bacterial strains *Pseudomonas aeruginosa* and zerovalent iron (Fe⁰) accelerated heavy metal reduction capacity for Cr(VI) and cadmium, 72.97% and 87.63%, respectively [94].

Pang et al. developed a synergistic system by immobilizing the Saccharomyces cerevisiae on the surface of chitosancoated magnetic nanoparticles (SICCM) for adsorption of Cu(II) from aqueous solution (Figures 9(a), 9(b), and 9(c)) [95]. After immobilization, magnetic adsorbent was pure Fe₃O₄ and it was without conglobation. Initial pH level of Cu(II) solution, concentration of Cu(II) solution, and application time were factors which influenced the final % removal of Cu(II). Highest adsorption potential was obtained at pH 4.5 (Figure 10). When initial dose of Cu(II) was 60 mg L-, then highest adsorption capacity obtained was 96.8% and this % removal efficiency increased as initial dose of Cu(II) increased (Figure 11). Equilibrium was obtained in 1 hour. The highest adsorption capacity for Cu(II) was assessed to be 144.9 mg g⁻. The tremendous feature of CCM for adsorption of heavy metals can be attributed to (1) high hydrophilicity due to large number of hydroxyl groups of glucose units, (2) presence of a large number of functional groups (acetamido, primary amino, so that it can absorb heavy metal ions in wastewater treatment and/or hydroxyl groups), (3) high tendency of these functional groups to react, and (4) flexible structure of the polymer chain.

Polyvinyl alcohol (PVA), sodium alginate, and multiwalled carbon nanotubes (MCNTs) were used by Pang et al. to immobilize a bacterial strain *Pseudomonas aeruginosa*. Prepared beads were kept at freezing temperature to improve its mechanical strength [96]. At 80 mg L⁻ Cr(VI) concentration, 50% Cr(VI) of its initial concentration was reduced in 84 hours. However, bacterial cells which were not immobilized became deactivate at this concentration. The beads were applied nine times for removal at 50 mg L⁻ Cr(VI) concentration. On first application, 90% removal was achieved, while in the end 65% removal efficiency was achieved (Table 2).

3.2.2. Reduction of Heavy Metals by Engineered Nanoparticles. Among natural reductant of Cr(VI), zerovalent iron is an alternative in the remediation of polluted sites, converting Cr(VI) to essentially nontoxic Cr(III). At $0.4\,\mathrm{g\,L^-}$ concentration of zerovalent iron, 100% of Cr(VI) (20 mg L $^-$) was reduced. Reduction potential of Cr(VI) suppressed markedly as initial pH increased. It was concluded that in each case Cr(OH) $_3$ should be the final product of Cr(VI) (1). In this way, iron nanoparticles are best option for the remediation of heavy metals in groundwater and soil [97]. Consider

$$CrO_4^{2-} + Fe^0 + 8H^+ \longrightarrow Fe^{3+} + Cr^{3+} + 4H_2O$$

 $(1-x) Fe^{3+} + (x) Cr^{3+} + 2H_2O$ (1)
 $\longrightarrow Fe_{(1-x)}Cr_xOOH_{(S)} + 3H^+.$

High removal efficiency of heavy metals and organic contaminants can be achieved by making amendments to

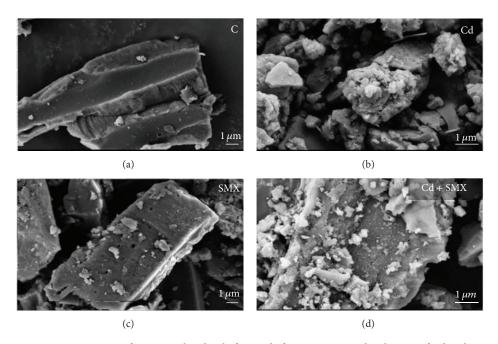


FIGURE 5: ESEM images of rice straw biochar before and after treatment with solutions of Cd and SMX.

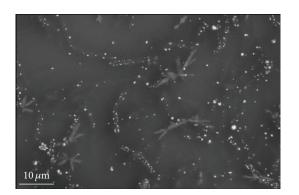


FIGURE 6: SEM image of bio-Pd(0) nanoparticles.

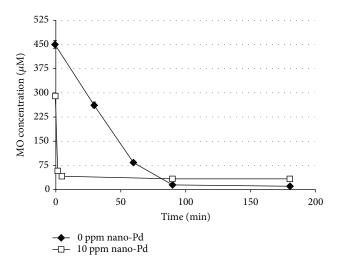


FIGURE 7: Concentration of methyl orange at different levels of bio-Pd(0) nanoparticles.

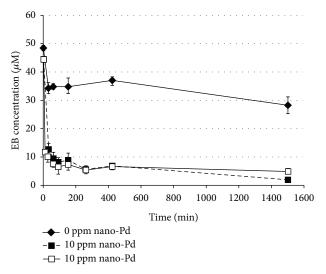


FIGURE 8: Concentration of Evan's blue at different levels of bio-Pd(0) nanoparticles.

NMs. For example, a novel magnetic nanosorbent (MNP-NH₂) has been produced by the covalent binding of 1,6-hexadiamine on the surface of Fe_3O_4 nanoparticles for the removal of Cu^{2+} ions from aqueous solution [98]. The chemisorptions occurred between Cu^{2+} and NH_2 groups on the surface of MNP-NH₂, as shown in

$$MNP-NH_2 + Cu^{+2} \longrightarrow MNP-NH_2Cu^{+2}. \tag{2}$$

In addition, the prepared nanosorbents had good reusability and stability, and the adsorption capacity of MNP-NH $_2$ was kept constant (about 25 mg g $^-$).

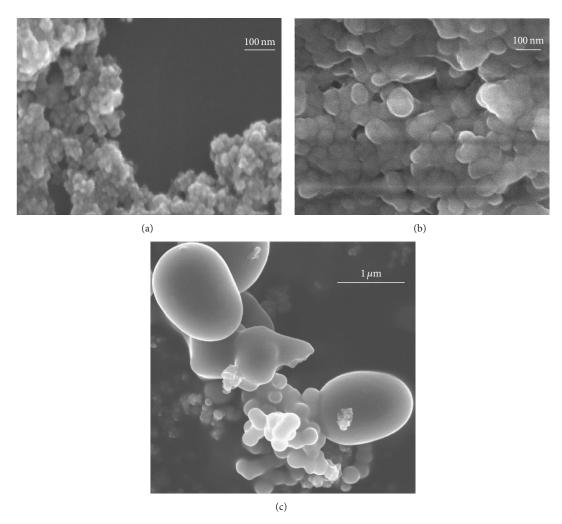


FIGURE 9: (a) Transmission electron micrograph of Fe_3O_4 magnetic nanoparticles and (b) chitosan-coated magnetic nanoparticles. (c) Immobilized *S. cerevisiae* on the surface of chitosan-coated magnetic nanoparticles.

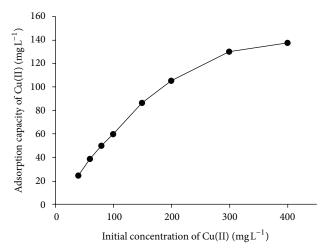


Figure 10: Adsorption capacities of Cu(II) mg L^- by *S. cerevisiae* immobilized on chitosan-coated magnetic nanoparticles at different initial concentrations of Cu(II) mg L^- .

Various forms of $\mathrm{Fe^0}$ were compared in the same conditions. The potential to degrade $\mathrm{Cr}(\mathrm{VI})$ was in the following order: starch-stabilized $\mathrm{Fe^0}$ nanoparticles > $\mathrm{Fe^0}$ nanoparticles > $\mathrm{Fe^0}$ powder > $\mathrm{Fe^0}$ filings (Figure 12). Figure 13 shows the ESEM images of the alone $\mathrm{Fe^0}$ nanoparticles (a) and starch stabilizer $\mathrm{Fe^0}$ nanoparticles (b). Much larger dendritic flocs have been formed without starch whereas discrete $\mathrm{Fe^0}$ nanoscale particles have been formed in the presence of starch (splinter-shaped crystalloid). The presence of starch effectively prevents accumulation of the iron particles and thus keeps high surface area and great reactivity [97].

Mesoporous gamma-Fe $_2$ O $_3$ nanoparticles possess superparamagnetic properties. It has comparatively great potential to remove Cr(VI) ions from the aqueous solution to that of pristine CMK-3 carbon. It was found that mesoporous gamma-Fe $_2$ O $_3$ nanoparticles (10 nm) had large adsorption capacity as compared to nonporous gamma-Fe $_2$ O $_3$ nanoparticles under same experimental conditions and degradation

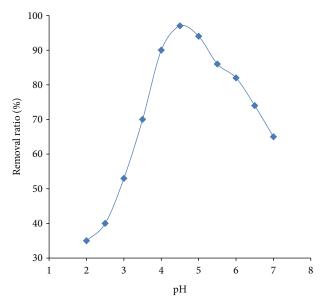


FIGURE 11: Removal ratio (%) of Cu(II) by *S. cerevisiae* immobilized on chitosan-coated magnetic nanoparticles at different pH levels.

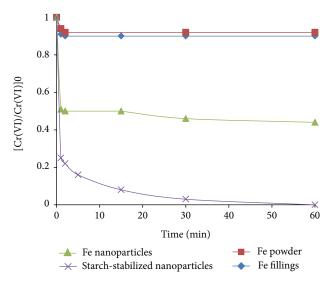


FIGURE 12: Concentration of Cr(VI) treated with different forms of Fe⁰ nanoparticles.

strength of mesoporous gamma- Fe_2O_3 nanoparticles for Cr(VI) increased as pH level of solution decreased [99].

Montmorillonite-supported magnetite nanoparticles were developed by coprecipitation and hydrosol method. The average sizes of the magnetite nanoparticles without and with montmorillonite support are around 25 and 15 nm, respectively. Adsorption potential of montmorillonite-supported magnetite nanoparticles was significantly higher per unit mass of magnetite (15.3 mg g $^-$) than that of unsupported magnetite (10.6 mg g $^-$) for heavy metal [100]. Similarly, bentonite-supported nanoscale zerovalent iron (B-nZVI) was prepared using liquid-phase reduction. Electroplating wastewater was treated with B-nZVI which exhibited higher potential to remove Cr, Pb, and Cu > 90% [20].

Nanoscale zerovalent iron- (nZVI-) multiwalled carbon nanotube (MWCNT) nanocomposites were applied to reduce Cr(VI) from wastewater. These were synthesized by embedding nZVI particles onto MWCNTs by in situ reduction of ferrous sulfate. The nZVI-MWCNT nanocomposites revealed around 36% higher reduction potential for Cr(VI) removal than that of bare nZVI or nZVI-activated carbon composites. Rate of removal of Cr(VI) increased at low pH and initial Cr(VI) concentration. Anions, such as $(SO_4)^{2-}$, NO_3^- , and HCO_3^- , exerted negative impacts on the removal of Cr(VI), while the influence of $PO_4^{\ 3-}$ and $SiO_3^{\ 2-}$ was not significant [101].

Li et al. developed silica fume-supported Fe(0) nanoparticles (SF-Fe(0)) that were prepared using commercial silica fume as a support [102]. The feasibility of using this SF-Fe(0) immobilized the Cr(VI) by adsorption on its surface following the reduction of Cr(VI) to Cr(III). The rate of reduction of Cr(VI) could be explained by pseudofirst-order reaction kinetics.

Surface engineered magnetic nanoparticles $\operatorname{Fe_3O_4}$ were produced by facile soft-chemical approaches. Nanoadsorbents were functionalized with carboxyl (succinic acid), amine (ethylenediamine), and thiol (2,3-dimercaptosuccinic acid). It has been suggested that nanoparticles formed in carboxyl, thiol, and amine functionalized $\operatorname{Fe_3O_4}$ have average sizes of about 10, 6, and ~40 nm, respectively. Rate of removal for heavy metals (Cr^{3+}), (Co^{2+}), (Ni^{2+}), (Cu^{2+}), (Cd^{2+}), (Pb^{2+}), and (As^{3+}) and bacterial pathogens (*Escherichia coli*) from water was highly efficient. Mechanism of removal of heavy metals involves the formation of chelate complexes or ion exchange process or electrostatic interaction depending upon the surface functionality (COOH, $\operatorname{NH_2}$, or SH) of magnetic nanoadsorbents [94].

It was explored by Wei et al. that magnetically iron-nickel oxide has great power for selective adsorption of Cr(VI) from the wastewater having Cr(VI)-Ni (II) [103]. The maximum adsorption capacity of Cr(VI) is about 30 mg g at pH 5.00 ± 0.02, and it was negatively correlated with total dissolved substance (TDS). Magnetic iron oxide nanoparticles were synthesized by a coprecipitation method followed by modification with 3-aminopropyl triethoxysilane (APTES) and acryloyl chloride (AC) subsequently. Then, the surface of modified nanoparticles was amended by graft polymerization with acrylic acid. The grafted magnetite nanoparticles exhibited great potential to capture heavy metal cations such as Cd²⁺, Pb², Ni²⁺, and Cu²⁺. Their size was in range of 10 to 23 nm. Adsorption capacity was reported to be 57.1 emu g [104]. Nanoscale δ -MnO₂ particles were embedded on the surfaces of GNS. It was found that GNS/MnO₂ have efficient capturing potential for Ni (II) from solution and it is 46.6 mg g at room temperature, which is 1.5 and 15 times higher than those of pure δ -MnO₂ and GNS, respectively [105].

Wastewaters often contain organics and heavy metals. Several experiments have been conducted to remove organic contaminants and heavy metals simultaneously using iron-based NMs stabilized on a surface. Currently, Long et al.

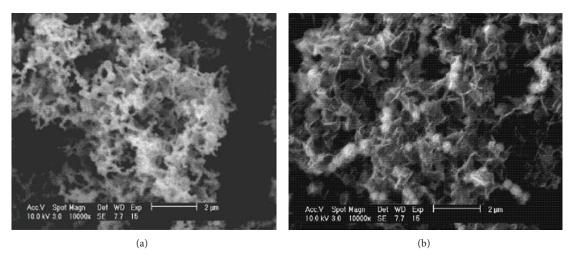


FIGURE 13: ESEM images of (a) alone Fe⁰ nanoparticles and (b) starch stabilizer Fe⁰ nanoparticles.

TABLE 2: Bio-nanocatalysts to remove heavy metals and organic contaminants.

Bionanocatalysts	Organic compounds	Heavy metals	Initial concentration of bionanocatalysts (ppm/mg L ⁻)	Initial concentration of heavy metals (mg l ⁻)		um reduction (%) Heavy metals		or maximum on (min/h) Heavy metals	References
[Bio-Pd(0) NMs] Pd(0) precipitated on <i>C. pasteurianur</i>	orange (M())	_	10 ppm	_	100%	_	7 min	_	[29]
Pd(0) precipitated on <i>C. pasteurianur</i>		_	5 ppm	_	100%	_	7 min	_	[29]
Bio-Pd(0) NMs	PCBs	_	$50\mathrm{mg}\mathrm{L}^-$	_	27%	_	_	_	[92]
<i>P. aeruginosa</i> immobilized (Fe ⁰)	_	Cr(VI)	_	_	_	72.97%	_	_	[95]
<i>P. aeruginosa</i> immobilized (Fe ⁰)	_	Cd(II)	_	_	_	87.63%	_	_	[92]
S. cerevisiae immobilized on chitosan-coated magnetic nanoparticles	_	Cu(II)	_	60 mg L ⁻	_	96.8%	_	1 h	[95]
P. aerugi- nosaimmobilized on multiwalled carbon nanotubes	_	Cr(VI)	_	$80~{ m mg}~{ m L}^-$	_	50%	_	84 h	[95]

synthesized chitosan-stabilized bimetallic Fe/Ni nanoparticles (CS-Fe/Ni) which efficiently reduced the amoxicillin by 68.9% and absorbed Cd(II) by 81.3% from a cocontaminated water [83], whereas separate reduction and adsorption rate for amoxicillin and Cd(II) were 93.0% and 90.9%, respectively, within 60 minutes. In this way, this remediation technique involves the reduction chemically and adsorption (Table 3).

3.2.3. Simultaneous Removal by Nanophotocatalysis. In this synergistic system, N-F-codoped ${\rm TiO_2}$ was used as a photocatalyst under visible light with enhanced photo efficiency to reduce ${\rm Cr(VI)}$ and benzoic acid (BA). Ratio of ${\rm Cr/BA}$

and concentration of N-F-codoped TiO_2 and pH were the selected variables, which effected significantly the removal of Cr(VI) and BA. Maximum degradation of Cr(VI) and BA was achieved at pH = 4, ratio Cr/BA = 5, and N-F-codoped $TiO_2 = 600$ mg L⁻. Reduction of Cr(VI) was suppressed as pH level increased, because of the anionic-type adsorption on TiO_2 and its acid-catalyzed photocatalytic reduction and the same trend was followed by BA. Figures 14 and 15 represent that, in binary system, no degradation was observed in the presence of only N-F-codoped TiO_2 after incubation for 240 min, whereas, in case of direct photolysis only, reduction of Cr(VI) and BA occurred at very slow rate. On the other hand, in single system, photocatalytic treatment completely reduced

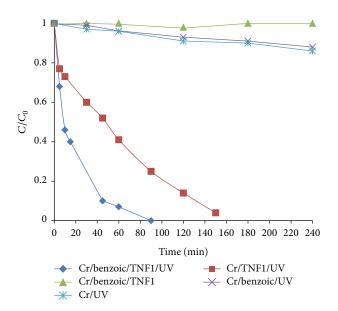


FIGURE 14: Photocatalytic reduction of Cr(VI) in single and binary system.

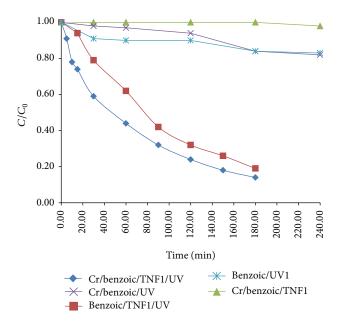


FIGURE 15: Photocatalytic reduction of benzoic acid (BA) in single and binary system.

Cr(VI) and BA after 150 and 240 min, respectively, while in binary system photocatalytic reduction of Cr(VI) and BA significantly boosted the oxidation/reduction of substrate and complete reduction of Cr(VI) maximum reduction of BA was achieved after incubation for 90 and 180 min, respectively. Mechanism for enhanced degradation includes the coupled oxidation of the BA that consumes photogenerated holes and/or *OH radicals efficiently, blocking the electron-hole recombination and, thus, increasing the total efficiency [38].

Moreover, the efficiency of (EDAS/TiO₂-Au) (nps) nanocomposite materials for photocatalytic oxidation and

reduction was assessed by applying them on Cr(VI) and methylene blue (MB) dye under irradiation. Deposition of Au nanoparticles on TiO_2 nanoparticles and then its spreading over silicate sol-gel film (EDAS/(TiO_2 -Au)) (nps) enhanced the photocatalytic reduction for Cr(VI) and oxidation of MB. Mechanism involves the most active interfacial electron transfer from the conduction band of the TiO_2 to Au (nps) by minimizing the charge recombination process when compared to the TiO_2 and (TiO_2 -Au) (nps) in the absence of EDAS [106].

Similarly, Doong et al. prepared metal-deposited Degussa P25 TiO₂ nanoparticles. Copper and silver ions were embedded on TiO₂ to accelerate photocatalytic degradation of methylene blue (MB) [107]. It was found that presence of formate stimulated the photocatalytic reduction of heavy metal ions by dropping its oxidation number and resulting in fast rate of photoreduction. In case of Degussa P25 TiO₂ nanoparticles, rate constant (k (obs)) for MB photodegradation was found to be $3.94 \times 10^{-2} \,\mathrm{min}^{-}$, whereas rate constant (k (obs)) increased by 1.4-1.7 times when metaldeposited Degussa P25 TiO₂ nanoparticles were applied. Concentration of heavy metal ions was also a factor which prompted the photodegradation of MB. Therefore, the rate constant reached up to $4.64-7.28 \times 10^{-2} \text{ min}^{-1}$ for Ag/TiO₂ and to $5.14-7.61 \times 10^{-2} \,\mathrm{min}^{-}$ for Cu/TiO₂. Furthermore, the electrons released from TiO2 may contribute to reducing heavy metal ions and MB simultaneously.

Simultaneous degradation of Cr(VI) and di-n-butyl phthalate (DBP) by UV/TiO_2 treatment was carried out by Xu et al. [65]. Concentration of Cr(VI) and DBP was significantly reduced and Cr(VI) exerted positive effect on DBP degradation and vice versa.

Similarly, simultaneous photocatalytic reduction/oxidation of Cr/salicylic acid was reported by Wang and Lo [108]. Both Cr(VI) and salicylic acid were successively reduced. It was investigated that when photocatalytic reduction of Cr(VI) was carried out for long time, it resulted in deposition of Cr(III) on the surface of ${\rm TiO_2}$ particles, which in turn deactivated the photocatalyst. However, this problem was overcome by oxidation of salicylic acid at the same time.

Peng et al. synthesized the polymer-sensitized TiO₂ for efficient reduction of Cr(VI) and oxidation of phenol simultaneously [109]. Poly(fluorene-co-thiophene) (PFT) showed the ability to reduce Cr(VI). When PFT was joined with TiO₂, not only it increased electron donor efficiency of PFT, but also it started to act as a sensitizer. This catalytic reduction of Cr(VI) was enhanced by the phenol existence. It was investigated by Tabassum et al. that the ultraviolet- (UVA-) induced photocatalytic application reduced the azo dye acid orange 20 (AO20) and Cr(VI) simultaneously [110]. The complete reduction was obtained after 120 min or 240 min at 500 or 250 mg \(\text{T}\) concentration of catalyst UV-induced TiO₂ at neutral pH. The synergistic effect of TiO₂ under visible light $(\lambda > 420 \text{ nm})$ to reduce the azo dye acid orange 7 (AO7) and Cr(VI), simultaneously, was extraordinary. Presence of metal ions enhanced the degradation rate of AO7. Similarly AO7 participated in increasing reduction rate of Cr(VI) [111].

A novel metal-semiconductor heterojunction with a tube-in-tube structure was synthesized by Luo et al. [112].

TABLE 3: Removal of heavy metals by surface stabilized nanomaterials (NMs).

Stabilized nanomaterials (NMs)	Heavy metals	Maximum removal %/mg L ⁻ /emu g ⁻	References
Starch stabilizer Fe ⁰ nanoparticles	Cr(VI)	_	[97]
Mesoporous gamma-Fe ₂ O ₃ nanoparticles	Cr(VI)	_	[99]
Montmorillonite-supported magnetite nanoparticles	_	_	[100]
Bentonite-supported nanoscale zerovalent iron (B-nZVI)	Cr(VI), Pb(II), and Cu(II)	>90%	[28]
Nanoscale zerovalent iron (nZVI)-multiwalled carbon nanotube (MWCNT) $$	Cr(VI)	_	[101]
Silica fume supported-Fe(0) nanoparticles (SF-Fe(0))	Cr(VI)	_	[102]
Surface engineered Fe ₃ O ₄	Cr(III), Co(II), and Ni(II)	_	[115]
Magnetically iron-nickel oxide	Cr(VI)	$30\mathrm{mg}\mathrm{L}^-$	[103]
Iron oxide nanoparticles modified with 3-aminopropyltriethoxysilane (APTES) and acryloyl chloride (AC)	Ni(II), Cr(VI), Pb(II), and Cu(II)	57.1 emu g ⁻	[104]
Nanoscale δ -MnO $_2$ embedded on graphene nanosheet	Ni(II)	$46.6~\mathrm{mg}~\mathrm{L}^-$	[105]
Chitosan stabilized bimetallic Fe/Ni nanoparticles (CS-Fe/Ni)	Cd(II)	90.9%	[83]

Table 4: Simultaneous removal of heavy metals and organic contaminants by nanophotocatalysts.

Synergistic system	Organic contaminants	Heavy metals		m removal %)	Removal n	nethod	Time for removal	maximum (min)	References
	Contaminants	inctais	O.C.	Heavy metals	O.C.	Heavy metals	O.C.	Heavy metals	
N-F-codoped TiO ₂ + visible light	Benzoic acid (BA)	Cr(VI)	Around 98%	100%	Oxidation	Reduction	90 min	180 min	[38]
EDAS/(TiO ₂ -Au) nps + radiations	Methylene blue (MB)	Cr(VI)	_	_	Oxidation	Reduction	_	_	[106]
$ \begin{tabular}{ll} Metal-deposited Degussa \\ (P25 TiO_2) nps + \\ radiations \\ \end{tabular} $	Methylene blue (MB)	Cr(VI)	_	_	Reduction	Reduction	_	_	[107]
UV/TiO ₂	Di-n-butyl phthalate (DBP)	Cr(VI)	_	_	_	Reduction	_	_	[65]
UV/TiO ₂	Salicylic acid	Cr(VI)	_	_	Oxidation	Reduction	_	_	[108]
Polymer-sensitized TiO ₂ + irradiations	Phenol	Cr(VI)	_	_	Oxidation	Reduction	_	_	[20]
UV-induced TiO ₂	Acid orange 20 (AO20)	Cr(VI)	100%	100%	Reduction	Reduction	120 min	120 min	[110]
UV/TiO ₂	Acid orange 7 (AO7)	Cr(VI)	100%	100%	Reduction	Reduction			[111]
Gold nanotubes embedded in pores of TiO ₂ nanotubes + radiations	Acid orange 7 (AO7)	Cr(VI)	_	_	Oxidation	Reduction	_	_	[112]

Gold nanotubes comprised of compressed and minute Au particles were deposited in the pores of anodic TiO₂ nanotube arrays by a simple pulse electrodeposition technique. An electric potential difference created at the interface of Au/TiO₂ heterojunction assisted the availability of photodegraded hole-electron, which in turn enhanced the photocatalytic activity. In binary system, Cr(VI) and AO7 reduced very rapidly because of synergistic effect of Cr(VI)-AO7 as well.

3.3. Simultaneous Biodegradation. Biological treatment is usually considered as an effective method and can significantly reduce the quantity of heavy metals in aqueous solutions. Few microbial strains have been isolated to reduce the organic contaminants and adsorption of heavy metals at the same time when cocultured. The most effective fungal strain *Phanerochaete chrysosporium* has been isolated by Chen et al. which can degrade the 2,4-dichlorophenol and adsorb the cadmium simultaneously in a cocontaminated wastewater [74]. Highest removal (%) was obtained at pH 6.5 of initial Cd(II) and 2,4-dichlorophenol doses

TABLE 5: Simultaneous biodegradation of organic contaminants and heavy metals.

Microbial etraine	Organic	Heavy	Initial level (mgl ⁻)	(mgl-)	% rer	% removal	Time for	Ϊ́	Temperature	Removal method	Deferences
	contaminants	metals	O.C.	Heavy metals	O.C.	Heavy metals	maximum removal		Ç	(O.C./heavy metals)	
P. chrysosporium	2,4- dichlorophenol	Cd(II)	20 mgl	5 mgl	83.90%	63.62%		6.5		Sorption/reduction	[64]
P. putida DMP-1 and E. coli ATCC 33456	Phenol	Cr(VI)								Reduction/reduction	[113]
P. putida DMP-1 and E. coli ATCC 33456 (Fixed film bio-reactor)	Phenol	Cr(VI)	840–3350 mgl ⁻	5-21 mgl ⁻	Almost 100%	Almost 100%				Reduction/reduction	[114]
P. aeruginosa CCTCC AB91095	Phenol	Cr(VI)	100 mgl ⁻	20 mgl ⁻	100%	100%	24/12 h (inocula 5% v/v)			Reduction/reduction	[27]
B. casei	Acid orange 7 (AO7)	Cr(VI)			40.7%	83.4%		_	35°C	Reduction/reduction	[16]
P. putida KI and S. proteamaculans SL14	Reactive black-5 (RB5)	Cr(VI)			100%	93%	24/12 h (individually)	7.2	35°C	Reduction/reduction	[23]

(5 and $20\,\mathrm{mg\,L^-}$), respectively. The reduction and sorption limit for 2,4-dichlorophenol and Cd(II) were 83.90% and 63.62%, respectively. Furthermore, degradation of 2,4-dichlorophenol was indicated by production of lignin peroxidase and manganese peroxidase in surplus amount (i.e., 7.35 U mL $^-$ and 8.30 U mL $^-$, resp.). However, production of protein was suppressed as the Cd(II) level increased.

In another experiment, cocontaminated wastewater was treated by combining two bacterial strains Pseudomonas putida DMP-1 and Escherichia coli ATCC 33456. These two bacterial strains rapidly reduced the Cr(VI) and phenol simultaneously. Reduction of Cr(VI) occurred by metabolism of E. coli. At small population size of E. coli, phenol degradation negatively affected the Cr(VI) degradation. Phenol degradation by P. putida was highly sensitive to Cr(VI) even at its low concentration, whereas phenol exerted inhibitory effect on Cr(VI) reduction only when phenol concentration was >9 Mm [113]. Similarly, Nkhalambayausi-Chirwa and Wang explored in an experiment that Cr(VI) and phenol can be reduced simultaneously by two bacterial strains Escherichia coli ATCC 33456 and Pseudomonas putida DMP-1, respectively, in a fixed-film bioreactor [114]. Almost 100% reduction of Cr(VI) and phenol degradation were achieved at initial concentrations (5-21 mg L⁻) of Cr(VI) and (840-3350 mg L⁻) phenol. Metabolites of phenol detected were 1. 2-hydroxymuconic semialdehyde (2HMSA), succinate, and acetate which contributed to increasing TOC by 13-23% in the treated wastewater.

By the development in biodegradation technology, remediation of Cr(VI) and organic contaminant simultaneously from wastewater and soil can be achieved by application of single microbial strain. Recently, simultaneous reduction of Cr(VI) and phenol has been carried out by application of only single strain for both contaminants. Song et al. isolated a fungal strain *Pseudomonas aeruginosa* CCTCC AB91095 [27]. Phenol served as a source of carbon and in turn energy produced was utilized for Cr(VI) reduction. Reduction of Cr(VI) and degradation of phenol was negatively influenced when Cr(VI) concentration was >20 mg L⁻ or phenol concentration was <100 mg L⁻. Nearly 100% reduction of Cr(VI) and phenol occurred after 24 hrs. The most effective concentration of inocula was 5% (v/v), at which Cr(VI) and phenol were abruptly suppressed from 20 and 100 to 3.36 and 29.51 mg L⁻ after 12 h.

Chromate Cr(VI) and azo dyes are common pollutants which may coexist in some industrial effluents. Therefore, few bacterial strains have been isolated which can reduce Cr(VI) and decolorize the azo dye simultaneously. A bacterial strain *Brevibacterium casei* was isolated from sewage sludge of a dyeing factory. Reduction of Cr(VI) and decolorization of azo dye acid orange 7 (AO7) simultaneously by application of *B. casei* were under nutrient-limiting condition, at pH 7 and 35°C. Chromate Cr(VI) and AO7 reduced by 83.4 \pm 0.6 and 40.7 \pm 1.7%, respectively. The mechanism of reduction involves that AO7 reduced by reduction enzyme(s) released from *B. casei* and AO7 served as an electron donor to reduce

Cr(VI) to Cr(III). In turn, Cr(III) formed a complex with oxidized AO7 and purple color appeared [16].

Currently, two potential bacterial strains *Pseudomonas putida* KI and *Serratia proteamaculans* SL14 were isolated from wastewater and sludge of tannery industry, capable of simultaneous reduction of Cr(VI) and decolorization of azo dye reactive black-5 (RB5). Maximum reduction of Cr(VI) and RB5 obtained was 93% and 100% after incubation for 24 h at pH 7.2 and 35°C. Individually, removal of Cr(VI) and RB5 was 100% after 12 h incubation (Table 5) [23].

4. Conclusions

Azo dyes and Cr(VI) most often coexist in industrial wastewater. These contaminants enter the environment when released through wastewater and exert many carcinogenic and mutagenic effects on plants, animals, and human health. Therefore, treatment of wastewater and its reuse is a practice related not only to a number of benefits with regard to eater balance and management but also to a number of question marks. Immediate research must be launched towards the direction so as to protect human health and environmental ecosystem. Microorganism (bacteria, fungi) are the potential source to remove these contaminants from soil and wastewater because they are cost effective and environmental friendly and remediate contaminants at faster rate. However, their immobilization can accelerate this treatment more efficiently. In this regard, surface modified nanomaterial and biochar have achieved much attention to remove heavy metals and azo dyes simultaneously. As illustrated in this review, a range of nanomicrobiological techniques have been proposed or are under active development for treatment of polluted soil and wastewater, but many techniques are still at experimental or pilot stage. In conclusion, there is much recent interest in the use of engineered nanomaterial combined with biotechnology as in in situ. In general, the attention in this field is not enough and additional studies should be conducted to increase the knowledge in this field. In addition, health impacts and environmental fate of these nanomaterials need to be addressed before their widespread application.

Conflict of Interests

The authors declare that there is no conflict of interests regarding the publication of this paper.

Acknowledgment

This research is supported by High Impact Research MoE Grant UM.C/625/1/HIR/MoE/SC/04 from the Ministry of Education Malaysia. Thanks also for the support by UMRG (RG257-13AFR) and FRGS (FP038-2013B).

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