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COST ANALYSIS OF DIFFERENT OPERATION STRATEGIES FOR FALLING PARTICLE RECEIVERS

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ABSTRACT

The potential for highly efficient and cost competitive solar energy collection at high temperatures drives the actual research and development activities for particle tower systems. One promising concept for particle receivers is the falling particle receiver. This paper is related to a particle receiver, in which falling ceramic particles form a particle curtain, which absorbs the concentrated solar radiation. Complex operation strategies will result in higher receiver costs, for both investment and operation. The objective of this paper is to assess the influence of the simultaneous variation of receiver costs and efficiency characteristics on levelized cost of heat (LCOH) and on levelized cost of electricity (LCOE).

Applying cost assumptions for the particle receiver and the particle transport system, the LCOE are estimated and compared for each considered concept. The power level of the compared concepts is 125 MW_{el} output at design point. The sensitivity of the results on the specific cost assumptions is analyzed. No detailed evaluation is done for the thermal storage, but comparable storage utilization and costs are assumed for all cases.

Keywords:

Concentrated Solar Power (CSP), Solid Particle Receiver (SPR), Falling Particle Receiver, Recirculation

INTRODUCTION

For solar tower systems, solid particle receivers (SPR) are considered as a promising concept to convert the solar radiation into heat. Ongoing research activities are based on the potential

of the technology that results from advantages over state-of-the-art technologies. Basically, SPR absorb the solar radiation directly in moving solid particles. The main advantages of SPR are

- Direct absorption by the particles, reducing the need for expensive high temperature materials.
- High operation temperatures possible (up to 1000°C).
- Adequate ceramic particles are commercially available.
- Particles can be used as absorber and storage material.
- High temperature spread and heat capacity allows high storage densities.
- Pressureless receiver design with open aperture possible.

Falling particle receivers (FPR) are a special kind of SPR, in which particles fall down gravity driven. In this paper only FPR are considered. Investigations regarding the FPR started in the 1980s at Sandia National Laboratories (1, 2). A small prototype was tested on-sun on the solar tower in Albuquerque in the early 21st century (8). Beyond the demonstration of the feasibility of a particle receiver, the experimental data was used for model validation (4, 5). Meier presented numerical studies on the particle flow behavior for a falling particle receiver/reactor for a cement production process (6). These investigations were related to a flat shaped particle curtain that was formed by particles, which fall downwards in a cavity. The apertures of the proposed cavities were located sidewise.

Another field of work is a cavity receiver, which has a downwards-facing aperture: the face-down receiver concept. The particles fall down in the cavity, located near to the inner

receiver walls. At the bottom the particles are collected by a collection ring.

So far, the face-down concept has only been evaluated theoretically for cubical and cylindrical cavities (7, 8, 9).

The advantage of this receiver concept is a reduction of convection losses due to the downwards-facing aperture, and the closed cavity, in which the hot air forms a stagnation zone (hot air in the upper part of the receiver, colder air in the lower part). This was quantified by using a CFD-model (8).

A specific problem of FPR occurs in part-load situations. When the incident solar power is reduced, the total particle mass flow must be reduced accordingly to maintain the desired particle outlet temperature. However, the reduced particle mass flow means an optically less dense particle film, resulting in lower overall absorption and higher reflection losses in the cavity.

In previous studies different operation strategies have been assessed to increase the receiver efficiency. To yield high part load efficiency, recirculation of particles was proposed (7). The two different operation strategies (with or without recirculation) are schematically shown in Figure 1.

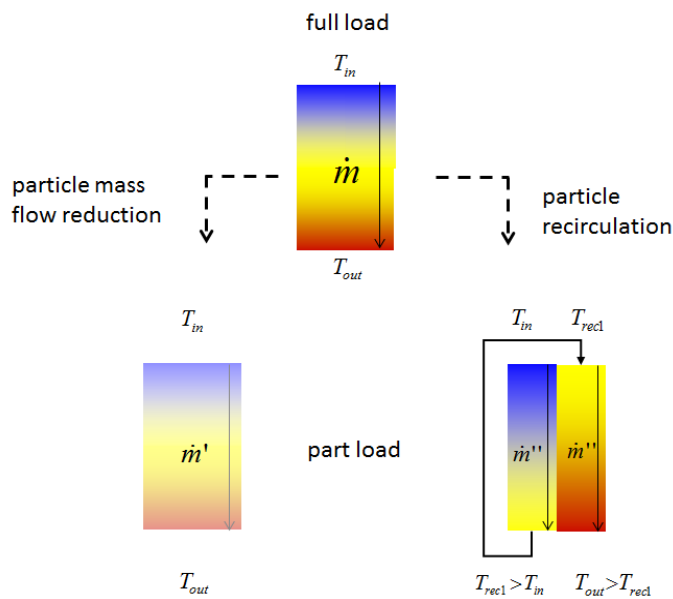


Figure 1: Top: operation under design point conditions (full load); bottom: part load operation strategies to yield same particle outlet temperature; left: operation without recirculation, mass flow reduction, low specific mass flow in cavity; right: operation with one recirculation, higher specific particle mass flow in cavity

In recirculation mode, the particle curtain is divided into several parallel sections. The particles are falling through each section, i. e. the drop more than once through the cavity. After each drop the particles are collected and circulated back to the inlet of the next receiver section. After the last section, the particles are exiting the receiver. Thus, the particles are heated

step by step to the receiver outlet temperature at the end of the last section. Since the particle mass flow in each section equals the total receiver mass flow, but at a significantly smaller curtain width, the particle curtain stays denser and the receiver losses due to reflection and emission can be reduced.

MODELING

For assessment of LCOH and LCOE system analysis were performed for operation with and without recirculation. The main focus of the system analysis was to determine the economic potential of the recirculation strategy.

The economic studies were based on common used tools and assumptions, which are described briefly in the following section “System Analysis”. Essential input data for the economic assessment are cost data, which are discussed in the section “Model Parameters” as well as the receiver efficiency characteristic curves. A summary of the methodology and assumptions for computation of receiver efficiency is given in section “Particle Receiver Modeling”.

System Analysis

The assessment is based on a modified and extended methodology of the European Concentrated Solar Thermal Roadmap (ECOSTAR) study and enables the prediction of the annual performance and the LCOE. The annual analysis uses as input an optimized heliostat field with optimized tower height, a receiver model with given aperture size considering its obtained efficiency characteristics (see next section), a piping model, using empirical correlations for the HTM flow in piping, a simplified storage model and 100% solar only operation strategy and a simplified model of the power block considering also the steam generator. The detailed model explanation of the used system analysis dataflow and sensitivity analysis is given in previously published literature (11,14). The overall assessment dataflow of the coupled tools is described in (12) and sketched in Fig. 2. In this context Fig. 2 depicts exemplary the connections of the relevant components and assumptions. For the heliostat field layout HFLCAL (10) and for the subsequent performance analysis and cost calculation the ECOSTAR methodology, which enables an hourly based annual performance and cost calculation, was used. The power block was modeled with the software Ebsilon. To be able to analyze a high number of system variations a master tool was programmed to automatically control the field layout, optimization, data transfer between the tools, annual analysis, system optimization and reporting of results. The advantages of this approach lie mainly in the simplified handling of the calculation process, reduced error rate due to user input errors and most of all net processing time.

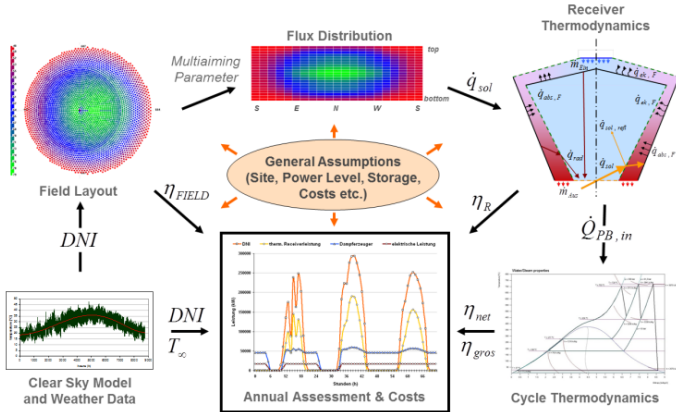


Figure 2: Sketch of the Annual Analysis Dataflow

Particle Receiver Modeling

Receiver efficiency characteristics were determined with a coupled CFD and ray tracing simulation for operation with and without recirculation and different solar loads. The receiver output power in design point was 355 MW_{th}. The receiver inlet temperature was set to 300°C and the desired particle outlet temperature was 800°C. In the following the modeling approaches are described briefly. Further information can be found in literature (9).

The proposed concept for the particle receiver was a falling particle curtain, which is falling down parallel to the inner wall of a cylindrical cavity. The particles collected at the bottom in a collection ring, which borders the open down-facing aperture. This so-called face-down cavity was simulated with numerical fluid dynamic simulation with the CFD-code (CFX). With a two-phase flow model the continuous fluid and discrete particles were simulated (Euler-Lagrange approach). Particle volume fraction distribution can be extracted from the CFD simulation result and used as input data for a ray tracing software, based on the SPRAY code. The principle for these subsequent ray tracing simulation is shown in Figure 3.

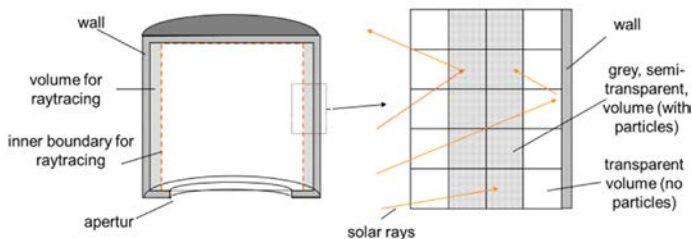


Figure 3: Principle of solar ray tracing for falling particle receiver modeling (left: half section of cylindrical face down cavity, right: of interaction between rays and volumes/faces).

As indicated in the schematic view in figure 3 the impinging rays can either

- be reflected by a particle loaded volume,
- be absorbed by a particle loaded volume,
- be transmitted through a particle loaded volume,
- be reflected by a wall,
- be absorbed by a wall, or
- leave the cavity through the aperture.

These quantities are determined statistically, depending on local particle volume fraction, properties of particles, and walls. So, with ray tracing simulation absorption of directional radiation from heliostat field in the particle loaded volumes and on receiver walls can be determined. Rays that leave the aperture are summed up to determine total reflection losses. The quantities for the absorbed radiation are used as input data for a sequential CFD simulation.

This CFD simulation includes:

- movement of the air (numerical fluid dynamics),
- movement of particles (discrete approach),
- momentum coupling between air and particles (Schiller-Naumann correlation),
- thermal radiation (diffuse, discrete ordinate model),
- convective heat transfer between wall and air (thermal wall function),
- convective heat transfer between air and particles (Ranz-Marshall correlation).

Particle mass flow rates were adapted to yield a temperature rise from 300°C to 800°C. Heat losses during recirculation were considered negligible. Windless conditions were considered for the presented cases.

Heating of the particles by the solar radiation leads also to heating of the air in the cavity. As a consequence, air properties and flow field in the cavity changes, which leads to modification of particle movement and volume fraction distribution. Thus, intermediate solutions were iterated between CFD and ray tracing until convergence was reached.

From a converged solution, receiver efficiency for one operation point can be determined. Receiver efficiency is defined as ratio of thermal output power to solar input power

$$\eta_{receiver} = \frac{\text{thermal output power from receiver}}{\text{solar input power into receiver}}$$

Receiver efficiency was determined in different load points and for operation with three subsequent recirculation steps and without recirculation to yield the efficiency characteristic curves. Computed receiver efficiencies in different load points were fitted with the following curves, to determine model parameters for yearly simulations. Figure 4 shows two

efficiency curves as function of input power relative to design point power (design point = 100%).

Main difference in efficiency is due to reduction of reflection losses. In design point reflection losses reduces from 9.8 to 2.2%. Because of higher transparency of the particle curtain at part load, the difference between the two cases increases, for example in excess of 10%-point at 50% part load.

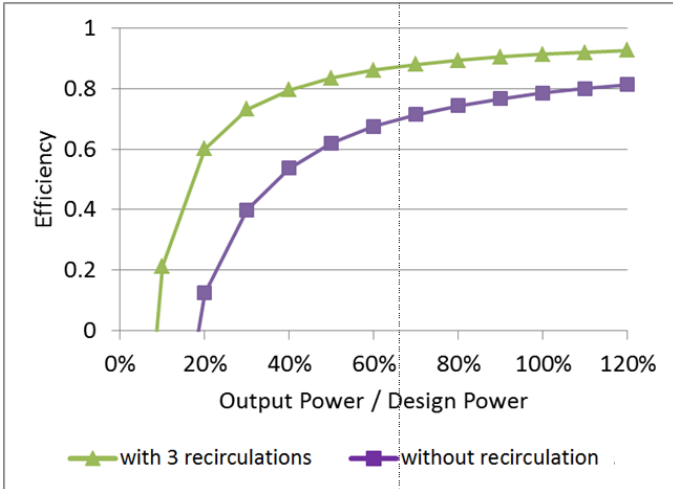


Figure 4: Receiver efficiency as function of input power relative to design point power (design point = 100%); for operation without recirculation and with three recirculations.

MODEL PARAMETERS

Model Parameters

The reference concept for the comparison here refers to a FPR without recirculation assuming a power level of 125MW_{el} . The site of the comparison is chosen to be Barstow ($34.85^\circ\text{N} / 116.8^\circ\text{E} / 600\text{m}$ above sea level / $\text{DNI at DP} = 901\text{W/m}^2$) while the design point (DP) is chosen to be March 21, 12:00 solar time. The main specifications of the reference concept are given in Table 1. For the receiver model, the particles were assumed to be gray with an absorptivity of 0.93 and the same value for emissivity. For the walls different values for solar absorptivity (0.25) and thermal emissivity (0.8) was assumed. These optical properties are in accordance with previous publications (2-5).

Cost Assumptions

The underlying cost assumptions for the annual analysis and assessment of LCOE are discussed below.

a) General Costs

General costs dataset is comparable to previous assessments (11, 12), where today's molten salt state-of-the-art technology was analyzed. Similarity is only considered for general costs dataset like heliostats or financing assumptions, which should be comparable. Differences to state of the art have been taken into account with a first best-guess for cost

Table 1: Main specification of the reference FPR concept

Solar Field	
Type	360° (surrounding field)
Reflective area of one heliostat	121 m ²
Effective reflectivity	89.34 %
Beam error	3.664 mrad
Solar multiple	2.5
Receiver	
Type	FPR in face-down cavity
Heat transfer medium (HTM)	sintered bauxite particles
Particle diameter	697µm diameter
Particle inlet temperature	300°C
Particle outlet temperature	800°C
Particle absorptivity (solar)	0.93
Particle emissivity (thermal)	0.93
Wall absorptivity(solar)	0.25
Wall emissivity (thermal)	0.8
Heat Transport System	
Type	Batch-transport in insulated containers
Heat tracing	Not necessary
Thermal Storage System	
2-tank direct storage	
Power block	
Type	Subcritical steam turbine
Life Steam Pressure	162 bar
Life Steam Temperature	550°C

assumptions. The general cost assumptions are listed in Table 2 and were discussed in the previous study related to increased receiver temperatures (12). Annual assessment also considers cost assumptions related to the labor costs per employee, number of persons for development, operation and the field maintenance, specific water cost, O&M Equipment costs percentage of investment annual insurance cost and service including equipment (for staff, water, etc.).

b) Particle Cycle

With the particle temperature of 800°C after the receiver and 300°C after the steam generator, a particle amount of 6.1 kg is needed per kWh of storage capacity. At particle costs of 1.2 \$/kg this corresponds to 7.3 \$/kWh for the particle inventory of the storage. A commercial offer for a smaller tank structure using high temperature steel as the tank shell and an outer insulation was extrapolated resulting in total specific storage costs of 18 \$/kWh_{th}. This number is a bit higher than the previously stated \$5–\$6/kWh_{th} for a particle storage system with very low cost particles and ceramic construction materials (13).

Table 2: Cost assumptions FPR system

a) General costs	
Components/ other costs	Costs*
Heliostats (incl. installation)	168 \$/m ²
Tower	300000 \$+ 17.72 \$ · HT2.39
Labor costs per employee	48000 €/year
number of persons (w/o field maintenance)	30
spec. number of persons for maintenance	0.03 per m ² heliostat
O&M Equipment costs (% of investment)	2 % per year
annual insurance cost (% of EPC)	0.3 %
service equipment (% of EPC)	2.5 %
indirect costs (% of EPC)	30 %
Financing (dept interest rate)	0.075
b) Particle Cycle	
Components	Costs ¹
Receiver (parameter variation)	12 to 204 \$/kW _{th}
Thermal Storage	15 €/kW _{th}
c) Balance of plant	
Components	Costs ¹
Power Block (without Stem Generator)	625 \$/kW _{el}
Steam Generator (parameter variation)	240 / 480 / 720 \$/kW _{el}

* cost assessment based on data in €, assumed exchange rate for cost data 1€=\$1.2

As actually no reliable cost data for falling particle receivers is available, a sensitivity study regarding the costs is presented, to show the influence of receiver costs and performance of the entire plant on the LCOE.

Receiver costs which include the particle transport system system were varied from 12 to 204 \$/kW_{th} as especially for the transport system cost numbers are still quite uncertain. Cost for the recirculation system (insulated containers and lift system) are not considered. Therefore, the difference between both case can be considered as economic limit for the additional costs of recirculation. Outer receiver wall structure is expected in the range of 12 \$/kW_{th} corresponding to the lower price range. Batch transport systems in the mining industry (skip hoists) with comparable transport capacities per height result in receiver costs of ~60 \$/kW_{th}. An upper limit of 204 \$/kW_{th} is chosen to reflect the handling of hot materials (insulated skip and hot input/output system) and the recirculation system.

c) Balance of Plant

The power block input data was provided by a turbine manufacturer and is confidential. Therefore only the relative economic comparison of the concept variants is carried out. Furthermore, to consider cost insecurities related to a steam generator that uses hot particles as the heat source the steam generator's cost are varied. Cost for power block without steam generator were assumed to be 625 \$/kW_{el}. This estimation is based on values known from literature (15,16).

Steam generator costs were varied between 240 and 720 \$/kW_{el}. This wide cost assumption range is chosen to cover high uncertainties related to a steam generator system that is driven by hot particles.

RESULTS

In Figure 5 the calculated LCOH related to both receiver concept options is depicted. The values are normalized to the case with recirculation and mean cost assumption. For the considered case, LCOH is 11-15% higher for the case without recirculation than for the case without, respectively 10 to 12%-points difference referred to normalized LCOH. With the present cost assumptions, up to 0.03 \$/kW_{th} can be saved, if for the FPR three recirculation stages are considered and if for both receiver concepts the same power specific costs are assumed. A FPR with three recirculation stages is allowed to cost up to 60 \$/kW_{th} more to reach the same LCOH like without recirculation stages.

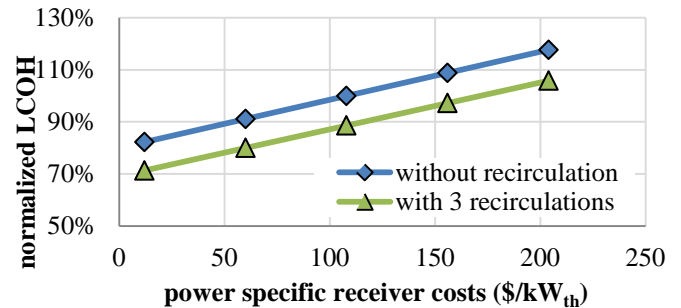


Figure 5: Normalized LCOH using an FPR with or without recirculation.

In Figure 6 the obtained normalized LCOE of both receiver concept options is shown. As additional parameter the specific costs of the steam generator operated by hot bauxite particles are varied between 240 and 720 $\$/kW_{el}$.

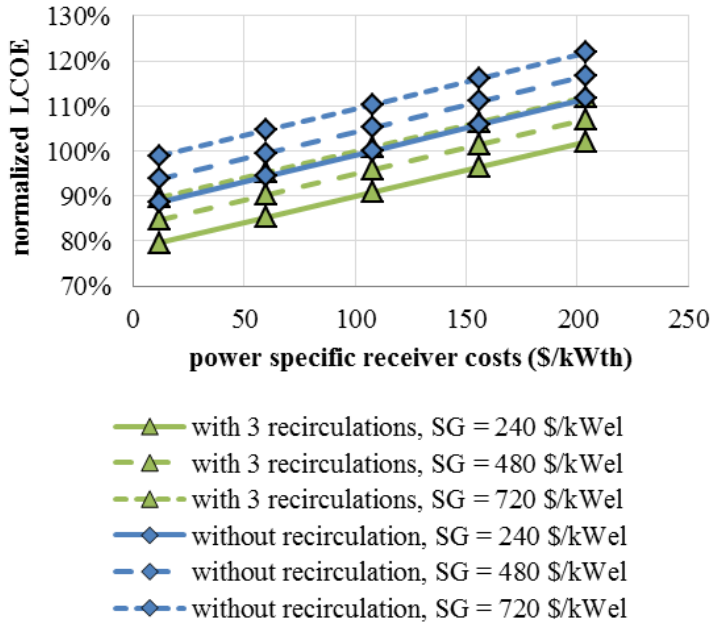


Figure 6: Normalized LCOE using an FPR with or without recirculation.

Up to 0.012 $\$/kW_{el}$ can be saved, if the FPR applies the considered recirculation stages independent from the costs of the steam generator. Furthermore it can be stated that for the assessed options a steam generator that costs 240 $\$/kW_{el}$ more leads to 0.006 $\$/kW_{el}$ higher LCOE. The optimal storage capacities of all assessed variants yield to 12h full load operation of the power plant. The approach of storage capacity optimization is carried out in two steps. First with a given range of solar multiples (SM) various system layouts take place. Then a parameter variation of the storage capacity is carried out. The storage capacity that leads to the lowest LCOE is taken as the optimal storage capacity corresponding to the assumed SM. The range of calculated annual component efficiencies lie in a ranges listed in Table 3.

Table 3: Ranges of calculated annual component efficiencies

Component	Costs
Solar Field	52.6 % - 56.3 %
Receiver	75.6 % - 82.9 %
Power Block (gross)	45.4 %
Power Block (net)	42.6 %
Whole Power Plant (net)	17 % - 19.7 %

CONCLUSION

Two different operating strategies for solar falling particle receivers were investigated and compared: without recirculation and with three-fold recirculation. Recirculation results in an optically denser particle film that reduces solar and thermal losses, thus achieving higher receiver efficiency. This is especially valid for part-load operation conditions.

On the other hand, recirculation means higher technical efforts and more equipment to transport the heated particles several times back to the particle inlet. Consequently, a receiver with recirculation will be more expensive. As the additional cost for recirculation is not known yet, a cost sensitivity study was made. In this study, the receiver cost as well as the cost for the particle steam generator was varied.

With optimized plant parameters and for specific receiver costs of 12 to 204 $\$/kW_{th}$ ¹, without recirculation the receiver efficiency decreases and with the same costs assumptions the LCOH increases 11 to 15% referred to the operation with recirculation. This gap is the “economic potential”, or in other words: higher costs for a receiver with a recirculation system should not overcompensate this efficiency advantage or the simpler receiver design has to reach a significant cost reduction to be competitive. To overcompensate the drawbacks in the efficiency characteristics the specific investment costs for the falling particle receiver have to be lower than 34 $\$/kW_{th}$ for this case.

Considering LCOE, a receiver with recirculation can be about 65 $\$/kW_{th}$ more expensive to achieve the same LCOE than a receiver without recirculation. Whether the additional equipment for recirculation can be built for this cost difference, is not known yet.

The variation of the particle steam generator cost shows similar trends in all configurations. An increase of steam generator cost by 480 $\$/kW_{el}$ results in an increase of the LCOE by about 0.012 $\$/kW_{el}$.

NOMENCLATURE

DNI	direct normal insolation
DP	design point
HTM	heat transfer medium
LCOE	levelized cost of electricity
LCOH	levelized cost of heat
FPR	falling particle receiver
SPR	solid particle receiver

ACKNOWLEDGMENTS

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¹ Parameter variation over wide range around Sunshot goal 125 $\$/kW_{th}$

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