

Nickel-free Hybrid Metal-Ceramic Supported SOFC

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Knowledge for Tomorrow

DLR German Aerospace Center

Aeronautics

Space

Transport

Energy

Space Agency

Project Management Agency

**Research
Institution**

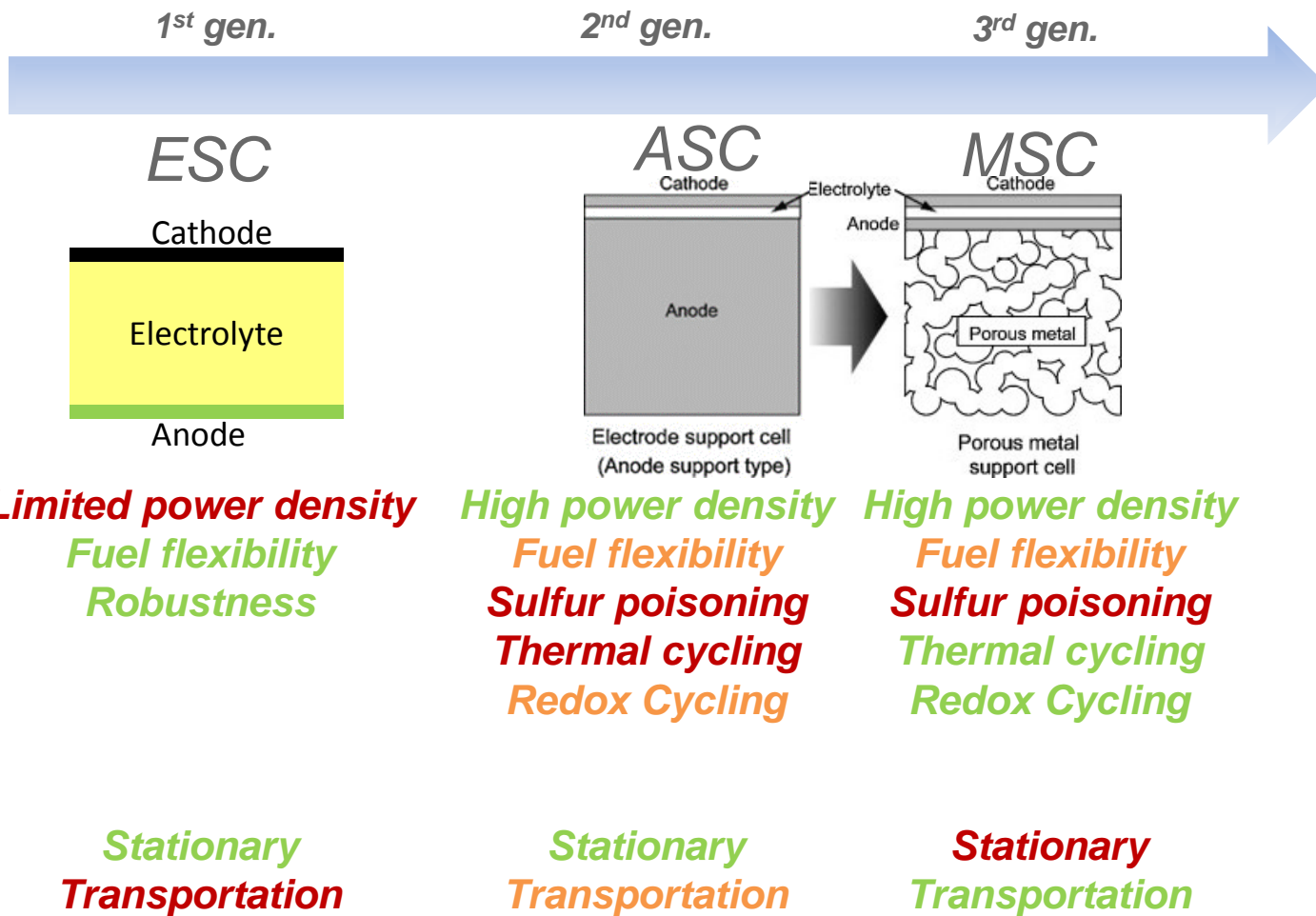


> 7500 employees across
32 institutes and facilities at
■ 16+1 sites.

Offices in Brussels, Paris, Washington.



Generations of planar SOFCs



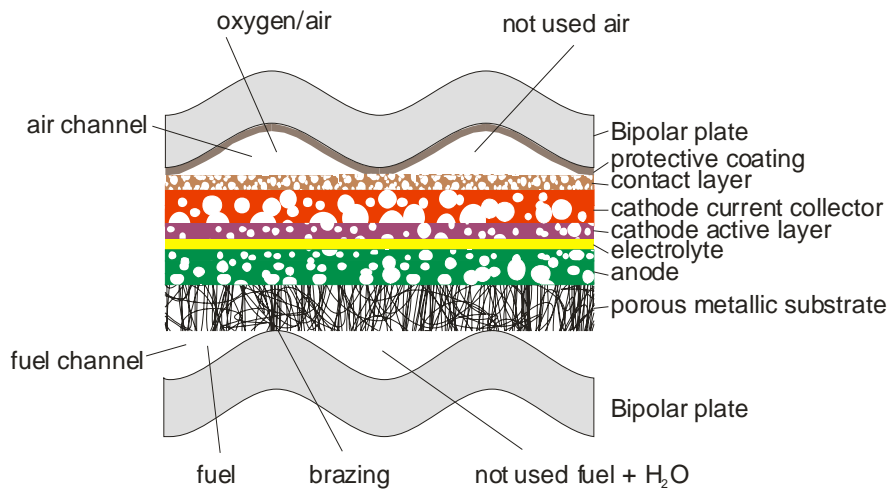
3rd Gen. SOFC: MSCs at DLR

Plasma Deposition Technology

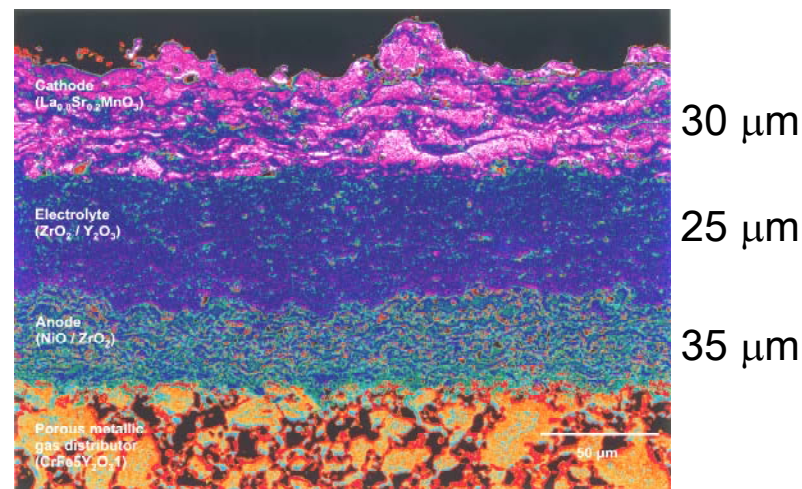
Ferritic Substrates and Interconnects

Compact Design with Thin Metal Sheet Substrates

Brazing, Welding and Glass Seal as Joining and Sealing Technology

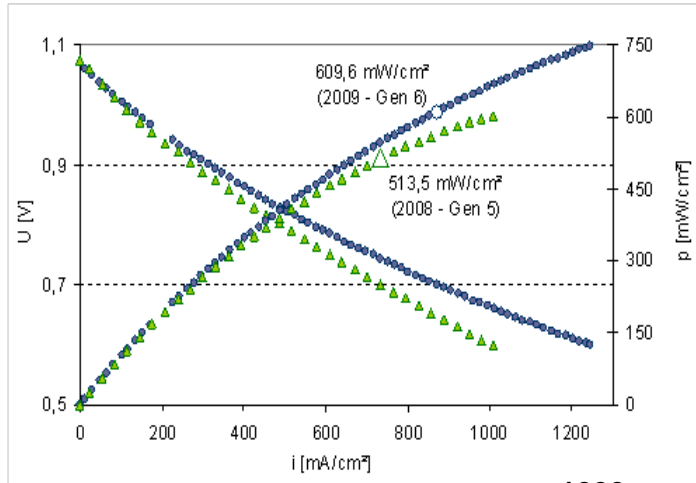


(not in scale)

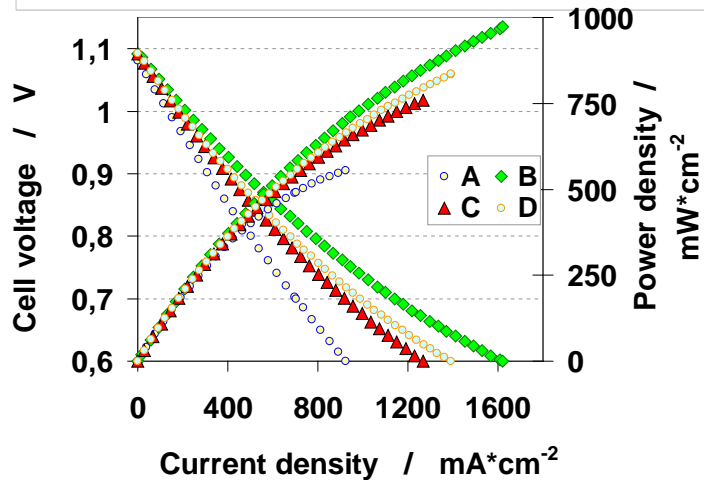




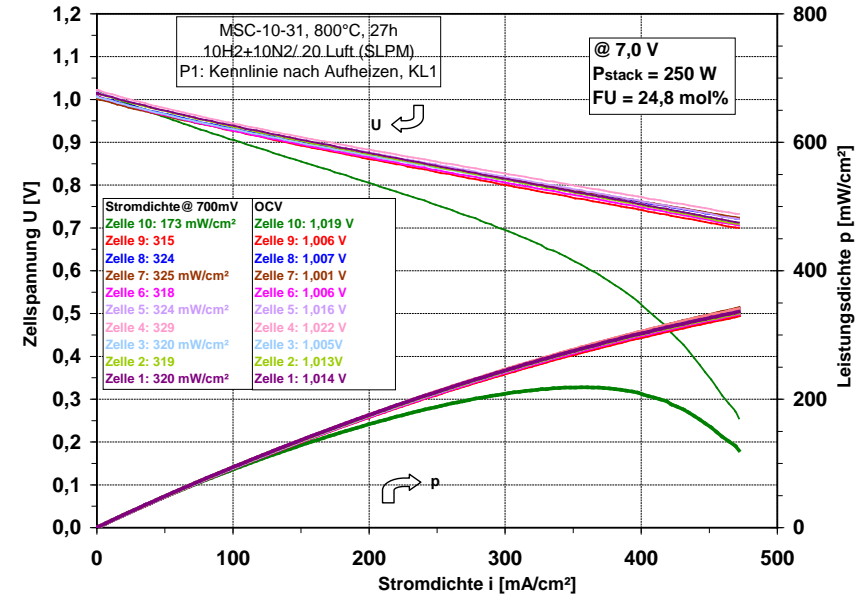
3rd Gen. SOFC: MSCs at DLR



APS



SPPS



10 Cells Stack

100 cm² single cells at 800°C; H₂/N₂; air

- P. Szabo, J. Arnold, T. Franco, M. Gindrat, A. Refke, A. Zagst, A. Ansar, *ECS Transactions*, 2009 (25) 2 p.175-185
- D. Soysal, A. Ansar, Z. Ilhan, R. Costa, *ECS transactions*, 2011 (35) 1 p.2233-2241



Beyond the 3rd Gen. SOFC: Issues to be addressed for improving MSCs

- **Cr-poisoning at the cathode side > Protective coating required**

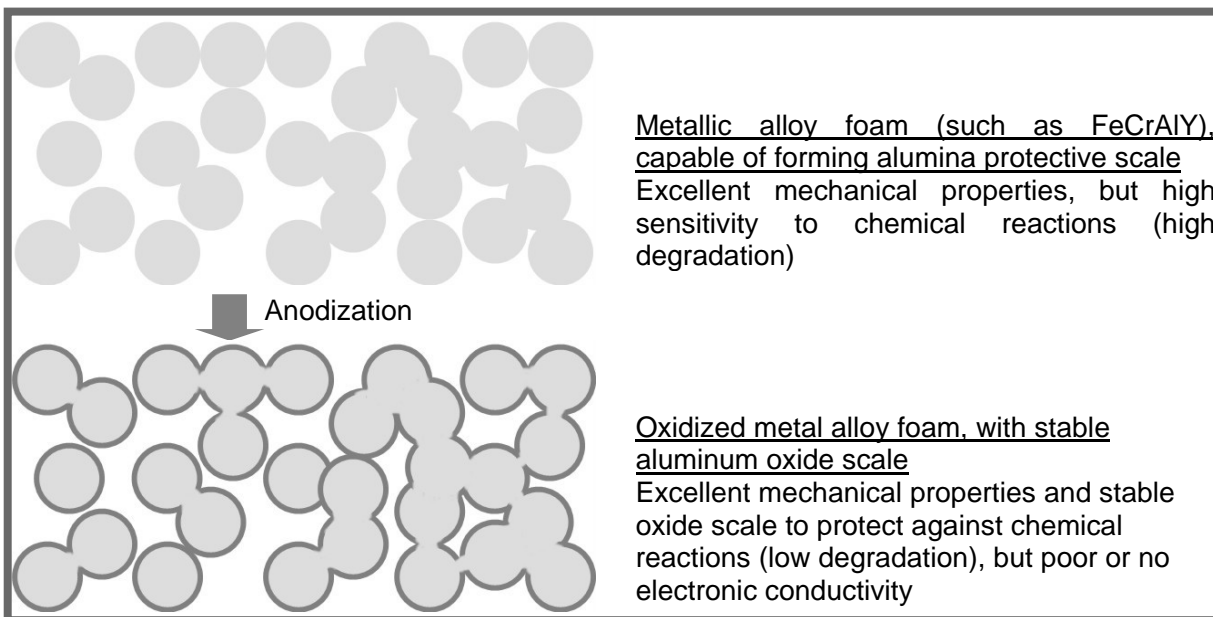
- **Improve tolerance toward sulfur poisoning**
- **Life time of metal substrate if stationary applications are considered**
- **Hermitic electrolyte**

Which materials and architecture
→ for the next generation of SO(F)C?



Nickel-free Hybrid Metal-Ceramic Supported SOFC

Metal substrate resistant toward oxidation

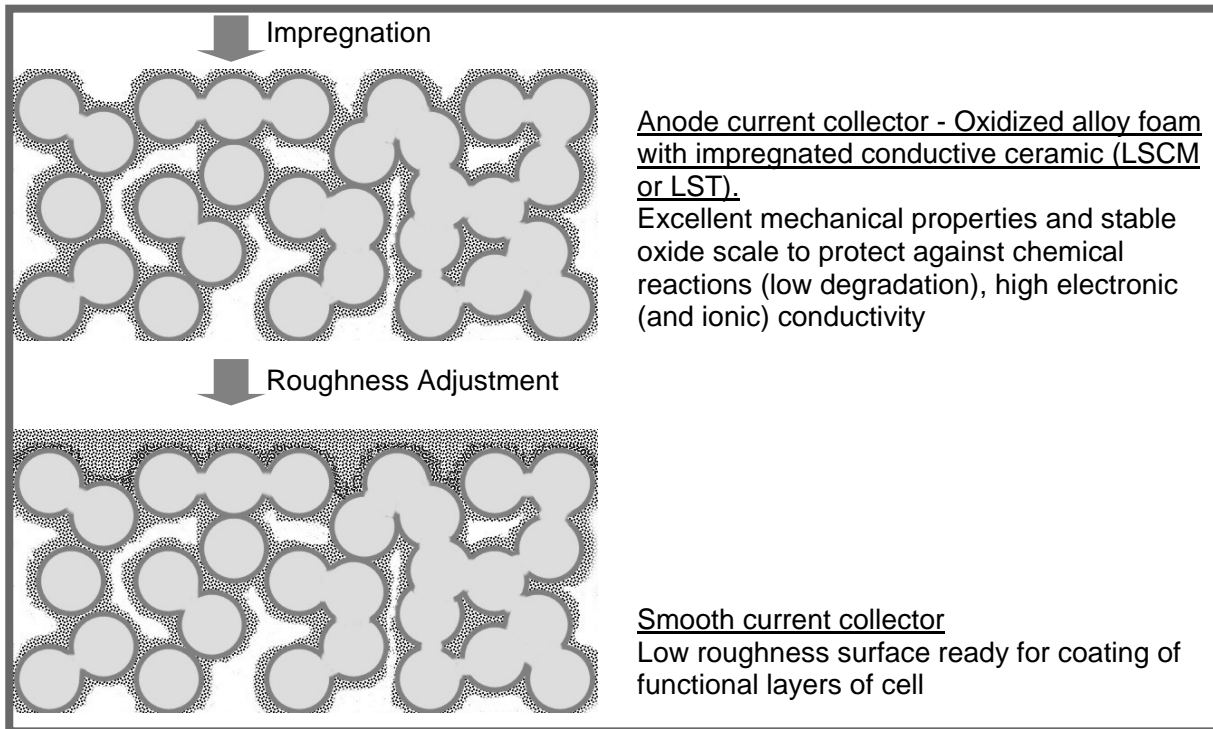


Formation of an Al_2O_3 layer as a durable protective coating

Al rich alloys, on the basis of $MCrAl(Y)$ with M being Fe, Ni, Co or a mixture



Nickel-free Hybrid Metal-Ceramic Supported SOFC



Infiltration with an electronic conductor (ideally a ceramic)
Target : 100 S/cm

Dense $\text{La}_{0.1}\text{Sr}_{0.9}\text{TiO}_3$ (800°C):
- sintering in H_2 : $\sigma_{\text{tot}} \approx 150 \text{ S/cm}$

O. Marina et al. Solid State Ionics, 149 (2002) 21-28.

S. Hashimoto et al. Journal of Alloys and Compounds, 397 (2005) 245-249.

Y. Tsvetkova et al. Materials and Design, 30 (2009) 206-209.

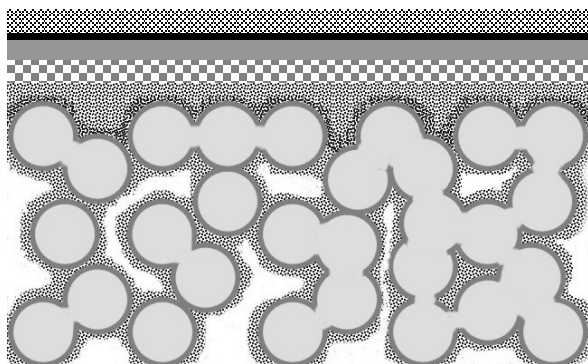
Hybrid current collector mechanically and chemically stable in both oxidant and reducing atmosphere









Nickel-free Hybrid Metal-Ceramic Supported SOFC

↓ Fabrication of functional layers on top of anode current collector+ infiltration



Realization of Evolve Cell

-  LSCF-CGO cathode
-  CGO diffusion barrier layer
-  YSZ or ScSZ Electrolyte
-  LSCM-CGO anode (with infiltrated Ni)

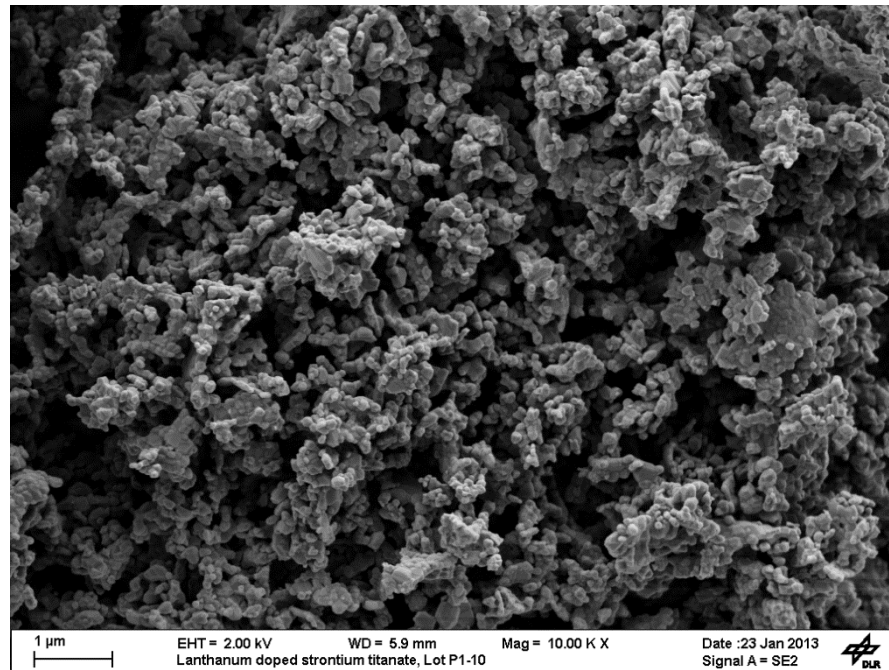
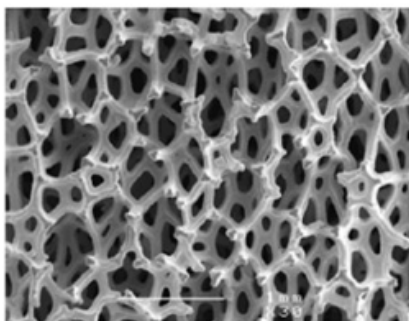
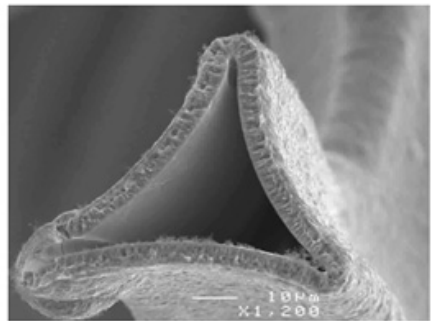
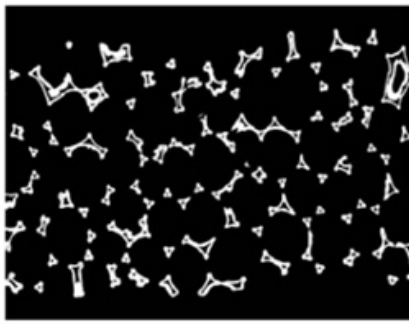
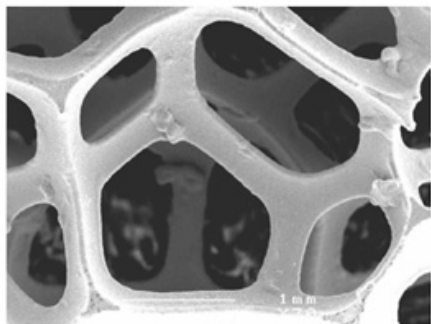
Use of perovskite materials at the anode and cathode, being modified by addition of suitable catalysts

High power density, Sulfur resistant, Fuel flexibility, Thermal cycling, Redox Cycling

Stationary applications ...



Nickel-free Hybrid Metal-Ceramic Supported SOFC



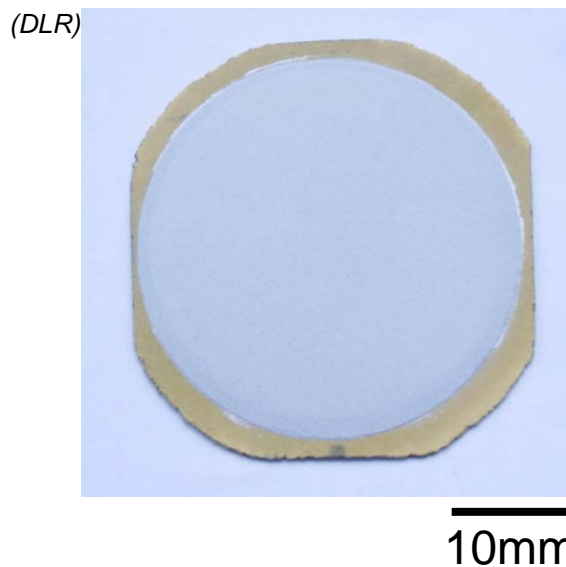
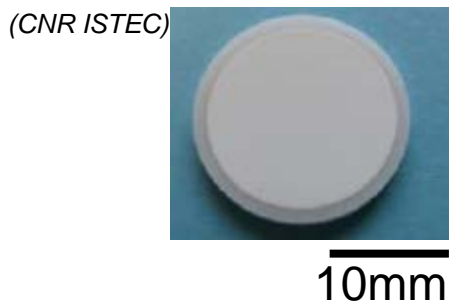
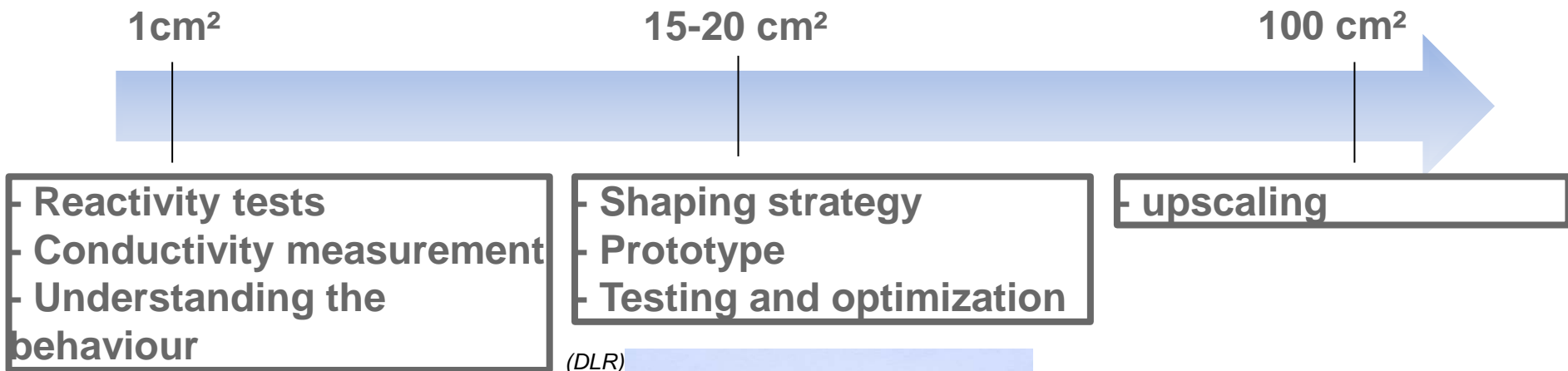
Composition of the anode: $Ce_{1-x}Gd_xO_{2-\alpha}$ / $La_{0,1}Sr_{0,9}TiO_{3-\alpha}$

Electrolyte: 8-YSZ

Cathode : $Ce_{1-x}Gd_xO_{2-\alpha}$ / $La_{0,4}Sr_{0,6}Co_{0,2}Fe_{0,8}O_{3-\alpha}$



Development strategy





Evaluation of the anodic electrocatalyst



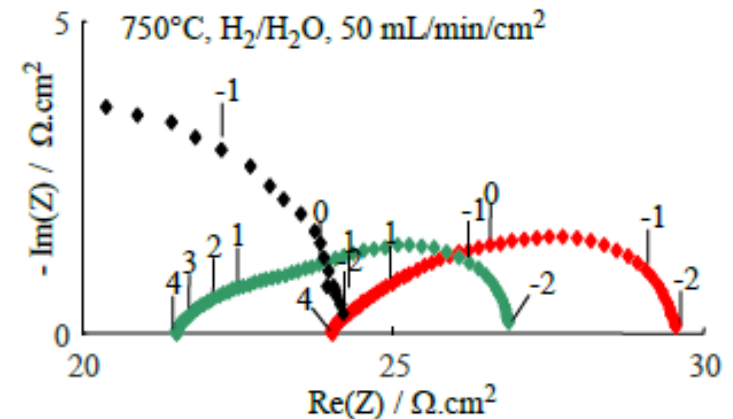
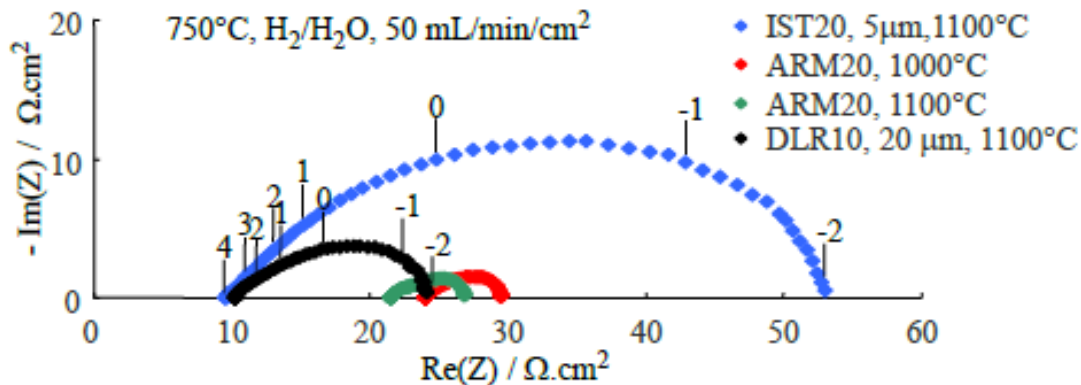
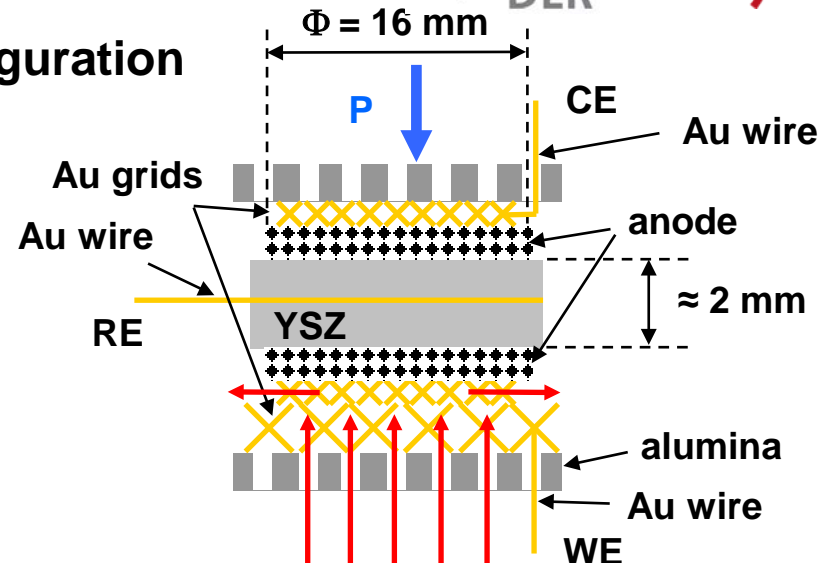
- Symmetrical cells tested in 3-electrodes configuration

- Experimental conditions

Gas composition, gas flow, Temperature

- Elaboration parameters

Composition, Thickness porosity



R_{po1} decreases: increase in thickness and/or decrease of the pore size



Electrokinetic modeling

• Reaction mechanism and kinetic data

Reaction	k^0	E^{act} (kJ·mol ⁻¹)
<i>LST/CGO phase</i>		
R1: $\text{H}_2 + 2 \text{O}_{\text{LST}} \rightleftharpoons \text{OH}_{\text{LST}} + \text{OH}_{\text{LST}}$	$1.5 \cdot 10^{14} \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	50.0
R2: $\text{H}_2\text{O} + \text{O}_{\text{LST}} + \square_{\text{LST}} \rightleftharpoons 2 \text{OH}_{\text{LST}}$	$1.0 \cdot 10^{18} \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	122.0
R3: $\text{O}_{\text{LST}} + \text{O}_{\text{LST}} \rightleftharpoons \text{O}_2 + \square_{\text{LST}}$	$1.0 \cdot 10^{22} \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	260.0
<i>YSZ/CGO phase</i>		
R4: $\text{O}_{\text{YSZ}}^{\times} + \text{V}_{\text{CGO}}^{\bullet\bullet} \rightleftharpoons \text{O}_{\text{CGO}}^{\times} + \square_{\text{CGO}}$	$1.0 \cdot 10^{22} \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	50.0
<i>Charge-transfer reactions</i>		
C1: $\text{O}_{\text{CGO}}^{\times} + \square_{\text{LST}} \rightleftharpoons \text{V}_{\text{CGO}}^{\bullet\bullet} + \text{O}_{\text{LST}}^{1-} + \text{e}^-$	$4.9 \cdot 10^{11} \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	129.0
C2: $\text{O}_{\text{LST}}^{1-} \rightleftharpoons \text{O}_{\text{LST}} + \text{e}^-$	$5.2 \cdot 10^3 \text{ cm}^2 \cdot \text{mol}^{-1} \cdot \text{s}^{-1}$	39.0

• Thermodynamic data

Species, i	h_i (kJ·mol ⁻¹)	s_i (J·K ⁻¹ ·mol ⁻¹)
<i>LST-CGO phase</i>		
\square_{LST}	0	0
O_{LST}	-85.6	139
OH_{LST}	-199.0	0
$\text{O}_{\text{LST}}^{1-}$	-114.0	139
$\text{O}_{\text{CGO}}^{\times}$	-236.0	0
$\text{V}_{\text{CGO}}^{\bullet\bullet}$	0	0
<i>YSZ phase</i>		
$\text{O}_{\text{YSZ}}^{\times}$	-236.0	0
$\text{V}_{\text{OYSZ}}^{\bullet\bullet}$	0	0

⇒ detailed multistep (electro-)chemical mechanism

⇒ thermodynamically consistent kinetic modeling

⇒ evaluation of main performance limitation processes



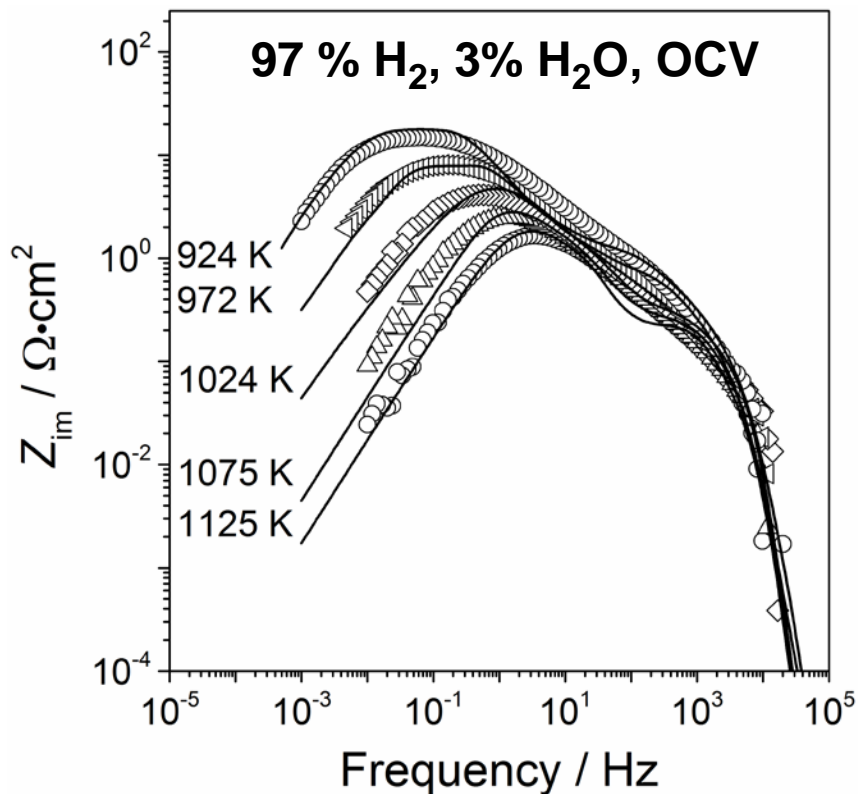


EVOLVE
FUEL CELL

Evaluation of the electrocatalyst



Electrochemical results: IST20



◆ LST-CGO20, 50 vol%-50 vol %
screen printing

◆ Data

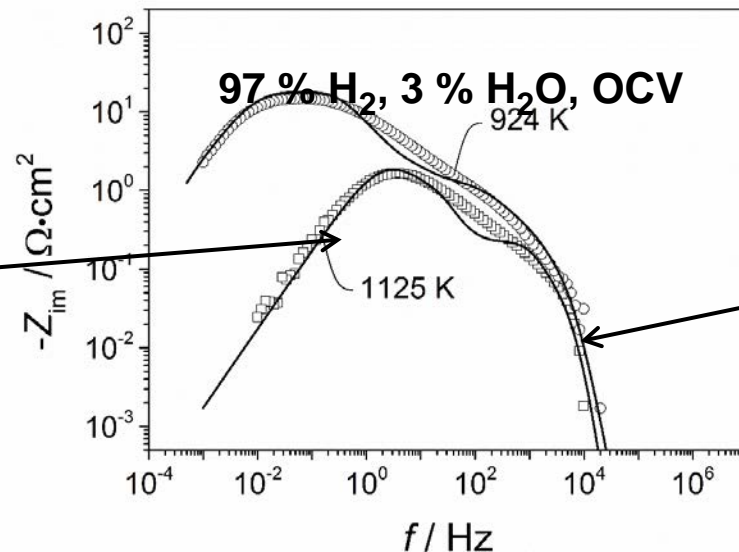
- Anode: 15 μm
- Electrolyte: 925 μm
- Mesh: 700 μm
- Inlet: 50 mL/min/cm²
- Active surface area:
4.6 10⁴ m²/m³

- ⇒ - **qualitative agreement between modeling and experiments**
- **three main impedance features**

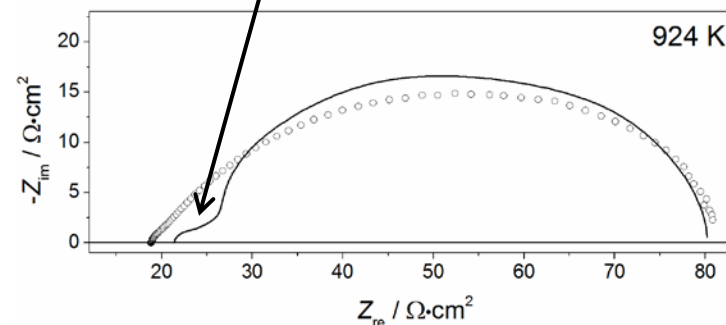
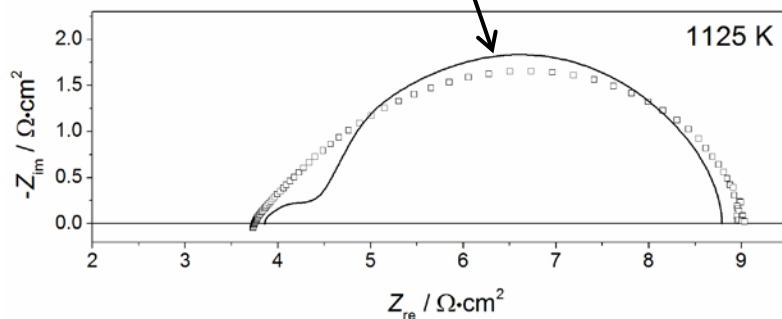


Evaluation of the electrocatalyst

surface
charge
transfer



interfacial
charge
transfer



- ⇒ - unambiguous assignment of impedance features
- influence of surface chemistry

Efficient LST based anodes requires high specific surface area



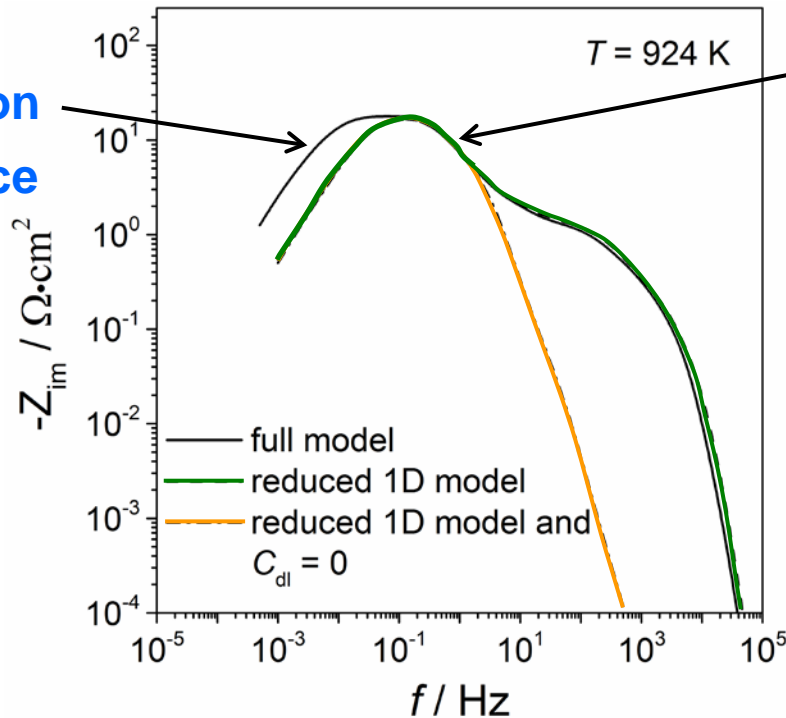


EVOLVE
FUEL CELL

Evaluation of the electrocatalyst



gas
conversion
impedance



H₂O
dissociation

Solid line:
full model

Dashed line:
reduced to 1D

⇒ **ideal supply channel transport**

Dashed-dotted line:
reduced to 1D with $C_{DL} = 0$

- ⇒ - **separation of transport and chemistry**
- **cell design optimization**

V. Yurkiv, G. Constantin, A. Hornes, A. Gondolini, E. Mercadelli, A. Sanson, L. Dessemond, R. Costa, submitted to Journal of Power Sources



Evaluation of the current collector

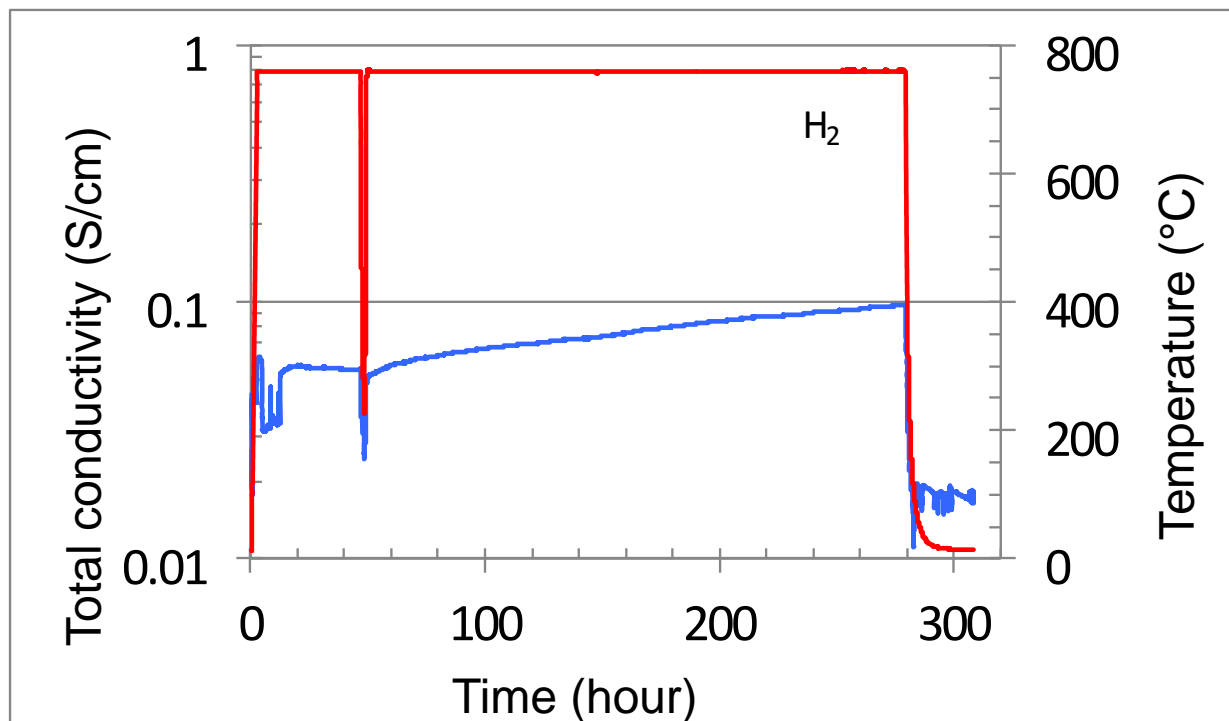




EVOLVE Evaluation of the current collector

FUEL CELL

**LST-NiCrAl current collector > Cathode sintering leads to full reoxidation of LST
Evaluation of in-situ reduction of LST during stack sealing/commissioning**



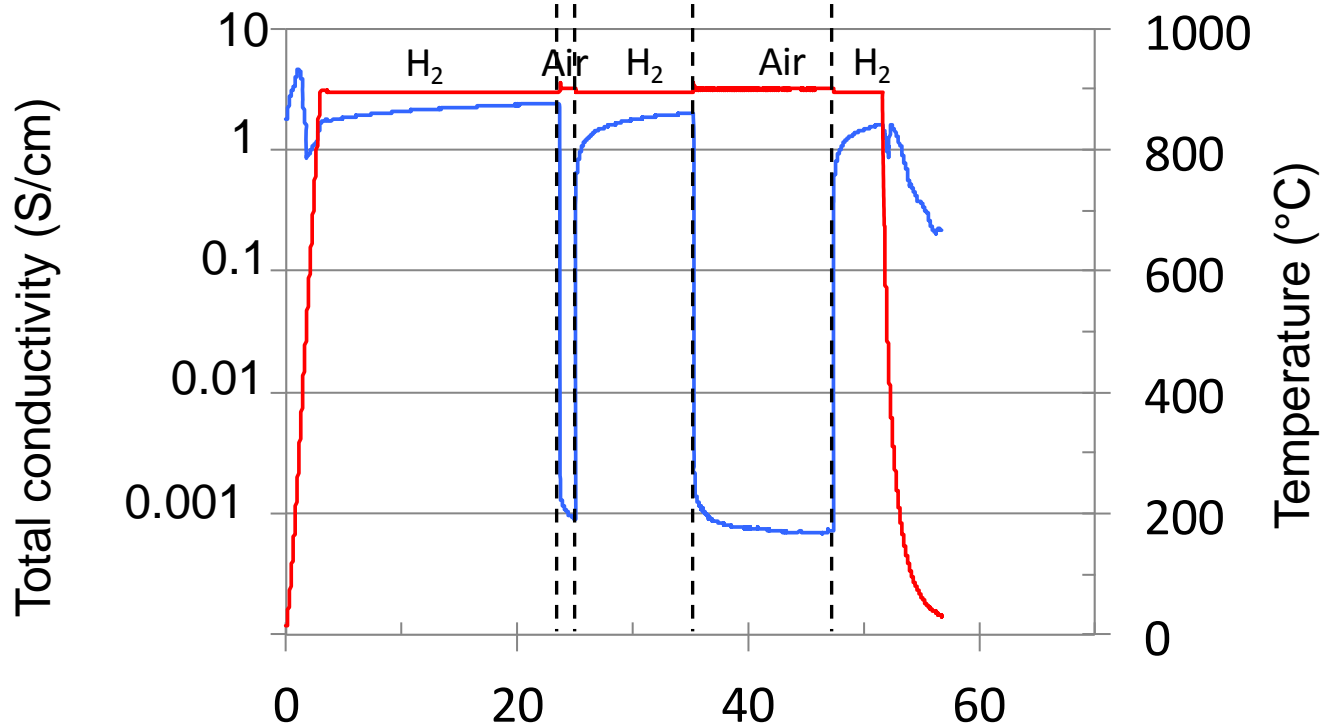
**Reduction at 750 °C
under H₂**

Total conductivity << 100 S/cm



Evaluation of the current collector

LST-NiCrAl current collector > Cathode sintering leads to full reoxidation of LST
Evaluation of in-situ reduction of LST during stack sealing/commissioning



**Reduction at 900 °C
under H₂**

Total conductivity << 100 S/cm



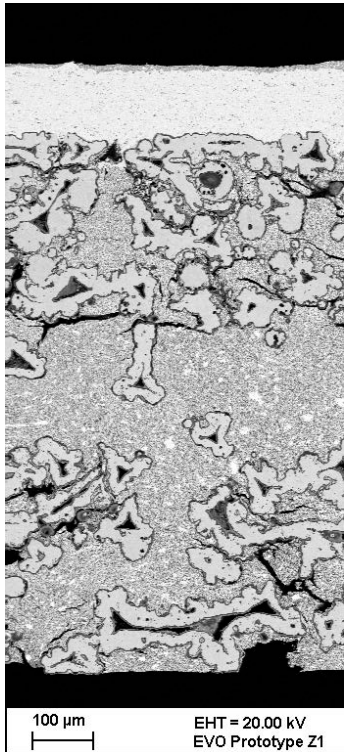
Full Cell Processing





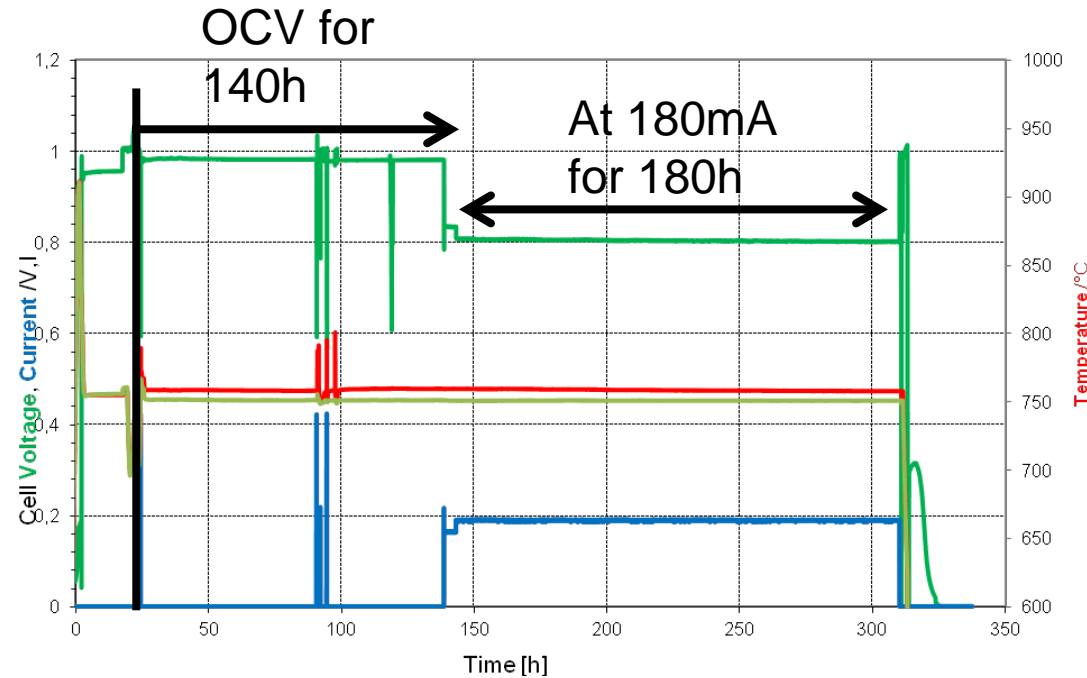
First demo Prototype through Plasma Spraying Route

Low risk approach using the know how from DLR for spraying YSZ layers. No need of sintering step.



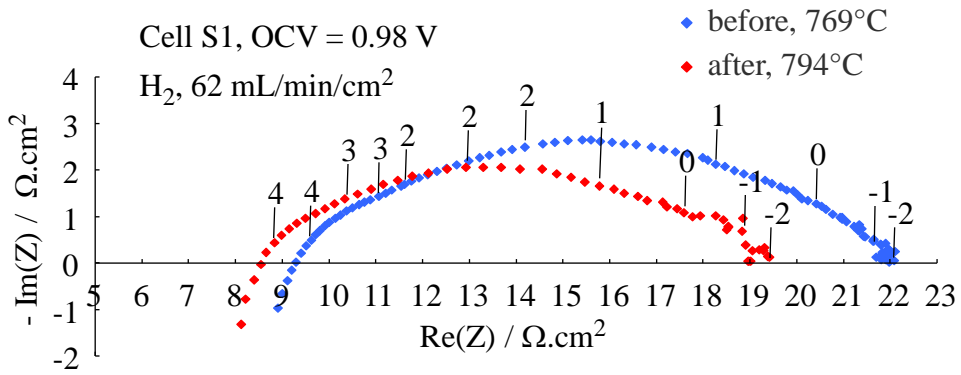
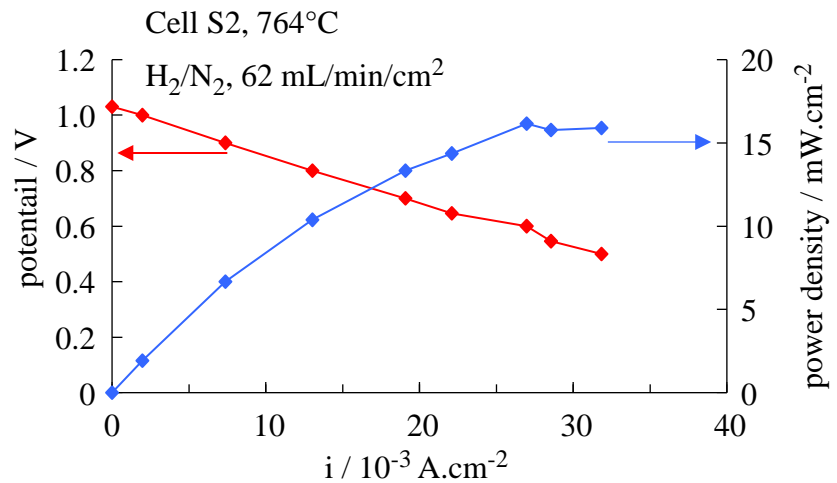
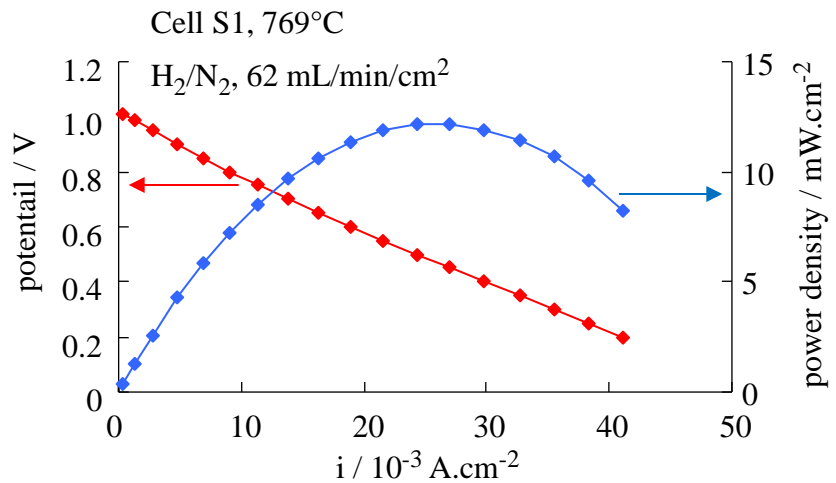
Cathode
100µm thick electrolyte

Co-pressed LST-CGO infiltrated NiCrAl foam





Prototype



- ⇒ - stable OCV and polarization curves for 50 hours
- 10-15 mW.cm⁻² at 0.7 V in H₂-air
- leakage (OCV_{exp} < OCV_{Nernst})

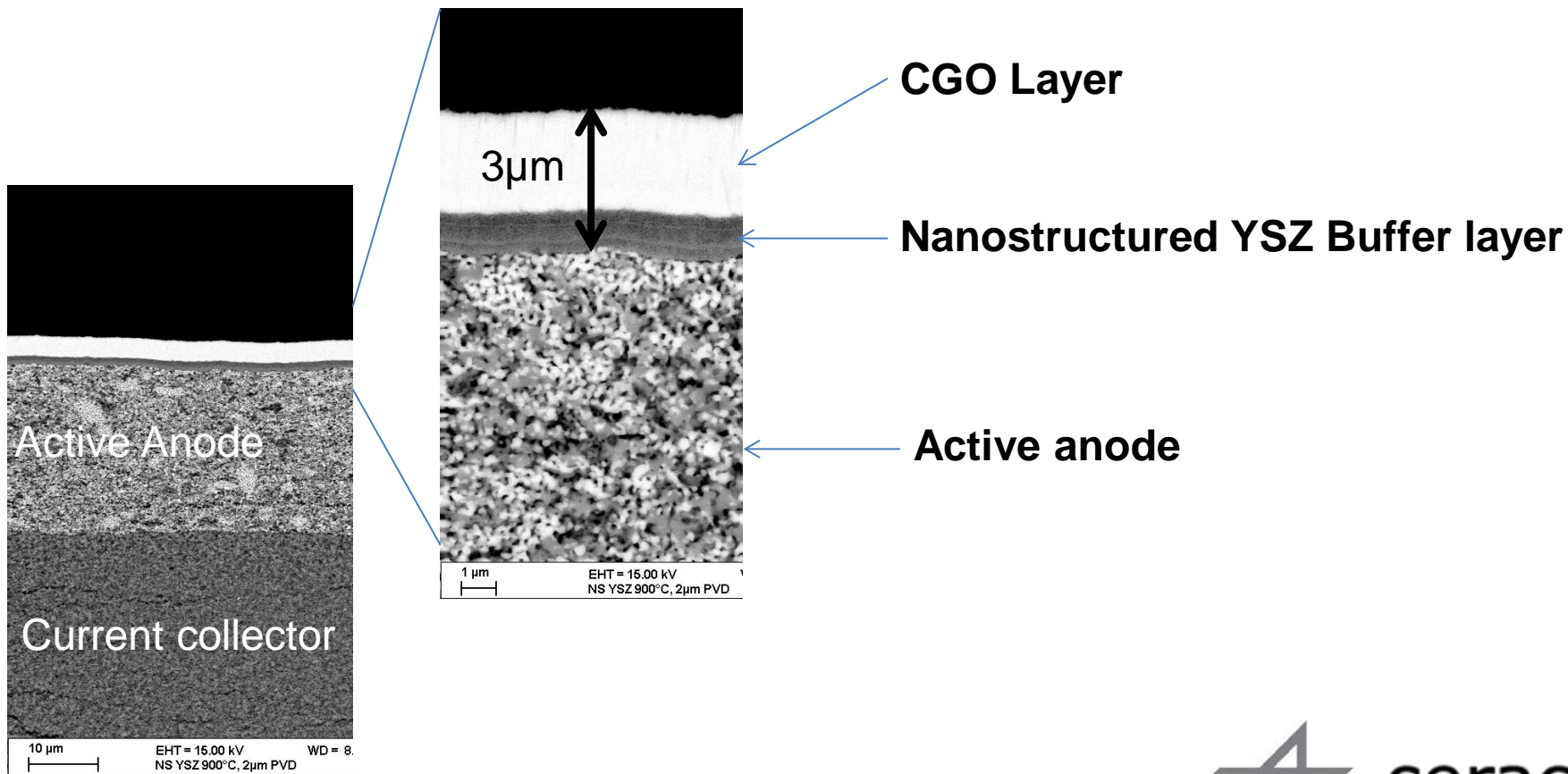




EVOLVE

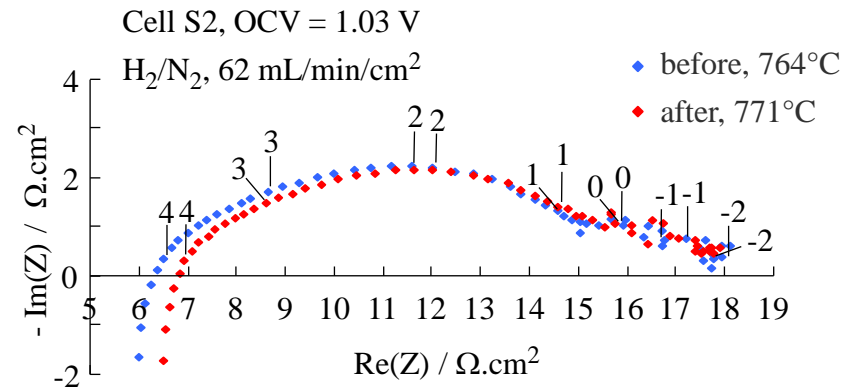
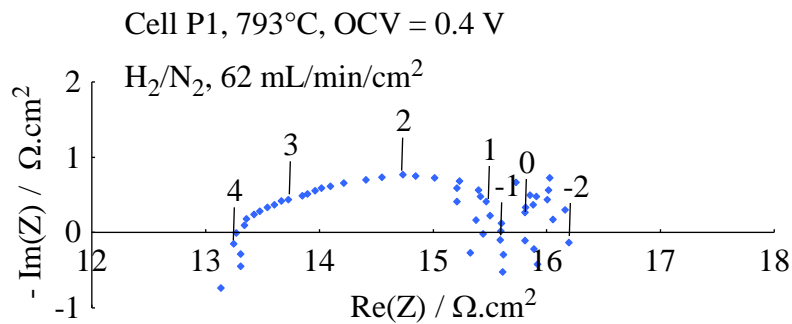
FUEL CELL

towards thin films electrolyte



EVOLVE *towards thin film electrolytes*

FUEL CELL



- Cell P:**
- low OCV
 - no polarization curves
 - high R_s but low R_{pol}



Conclusion & perspectives

- $La_{0,1}Sr_{0,9}TiO_{3-\alpha}$

Requires high specific surface area
Requires specific treatment for full activation

- *Reducibility and maximum level of perovskites electrocatalysts needs to be enhanced*
- *Implementation of metals seems necessary to achieve conductivity target in the current collector*

> demonstration up to 100cm² cell of SOC



Acknowledgement

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Thank you for your attention!

