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13 Laboratory scale geophysical measurements aimed at monitoring the

14 thermal affected zone in Underground Thermal Energy Storage (UTES)

15 **applications.**

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24 Abstract

25 Underground Thermal Energy Storage systems have showed to be a useful and increasing technical solution for covering the heating and cooling and domestic hot water buildings' demand. Thermal 26 influence of these plants is however not still debated as it deserves and correct monitoring strategies 27 28 appear to be of major importance both to better understand processes and to highlight their 29 environmental effects into high populated areas. Litho-, hydro- and bio-sphere can indeed be adversely affected by temperature variations induced in the underground by heat storage applications. For this 30 purpose, a geophysical approach using time-lapse electrical resistivity measurements contemporary to 31 analogical simulations is here tested at laboratory scale. Results of the experiments are reported 32 comparing measured apparent resistivity with direct temperature measurements and numerical 33 simulations of heat propagation. Data presented confirmed that electrical resistivity has powerful 34 relation with temperature variation in monitored media. In addition, they showed that also without 35 performing data inversion valid temperature estimation can be carried out. Post processing calibration 36 of apparent resistivity data showed to be in acceptable agreement with both temperature measurements 37 and numerical simulations. Simple apparent electrical resistivity variations appear therefore to be a 38 promising, economic, quick and non-invasive tool for mapping thermal modifications induced in the 39 underground by shallow geothermal applications. 40

Keywords: apparent electrical resistivity; numerical simulation; analogical modeling; porous media;
 shallow geothermal applications.

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56 1. INTRODUCTION

The idea of exploiting the thermal energy provided by renewable sources has been always 57 related to the problem that most of these sources supply energy when the user's demand is low 58 (e.g. sun energy is related to the warm season, when the heating demand is reduced). In this 59 respect, the thermal energy storage is a highly debated concept since the late 70s; several 60 Underground Thermal Energy Storage (UTES) technologies have been developed in recent 61 years to find some new solutions assuring criteria of reliability, efficiency and economic 62 sustainability. Short-term (daily) and long-term (seasonal) storages are the two main categories 63 discriminating the storage mechanism, depending on the duration of the storing activity. The 64 seasonal storage seems to satisfy the annual heat demand better than the short-term, with a 60% 65 against a 20% of total energy demand provided (Fisch et al., 1998; Sanner, 2003; Xu et al., 66 2014). It is however true that the seasonal storage implies bigger economical investments and 67 wider storage volumes, hence it results in a more challenging technology in terms of storing 68 materials, heat loss evaluations and environmental impact reductions. 69

UTES systems are based on the sensible heat storage mechanism which is considered to 70 71 be a simple, low-cost, more reliable and acceptable technology compared to other alternatives (latent heat or chemical reaction/thermo-chemical sorption), even if the latter have higher 72 energy storage densities (for detailed discussion refer to Xu el al., 2014). Several methodologies 73 are available depending on the storing medium: (ATES – Aquifer Thermal Energy Storage) 74 (Rosen, 1999; Paskoy et al., 2000; Dickinson et al., 2009), hot water confined in steel tanks 75 (Novo et al., 2010; Schmidt et al., 2004) or the ground itself; in this last case the connection 76 with the ground is provided by a series of boreholes heat exchangers (BTES - Boreholes 77 Thermal Energy Storage) (Bakema et al., 1995; Fisch et al., 1998; Reuss et al., 2006; DLSC, 78 2012; Giordano et al., 2016). 79

Mainly ATES and BTES have therefore geological implications. In both cases, thermal 80 and hydrogeological properties of the ground have to be taken into account for the design and 81 operation of the installation. Both storage systems have a strong environmental impact: a big 82 part of the aquifer could be influenced in the first case, a noticeable underground volume is 83 interested by drilling activity in the latter. In any case a not negligible Thermal Affected Zone 84 (TAZ) is generated and an accurate monitoring activity must be considered to take care of the 85 possible negative effects induced on litho-, hydro- and bio-sphere. Generally, an accurate study 86 of the thermal behavior of the storage medium and a correct monitoring of TAZ are also useful 87 to understand processes. 88

So far, there is limited specific knowledge about the effects of unsuitable system design 89 (e.g. unwanted temperature and chemical changes within the subsurface and resulting 90 consequences). Only few studies have measured the thermal effects of low enthalpy geothermal 91 applications within field sites. Arslan and Huber (2013) compared field temperature 92 observations with numerical simulations and laboratory measurements under a forced 93 groundwater flow. Lo Russo et al. (2014), evidenced that the thermal plumes generated by well 94 doublets of groundwater heat pumps can be regarded either as a potential resource or as a 95 pollution. Bonte (2013) studied temperature-induced impacts on the groundwater quality, 96 accounting for variations in the mobility of trace elements, redox processes and microbial 97 communities. Most studies agree that a 10°C temperature change can be sufficient to stimulate 98 trace elements mobility and microbial activity variations. Considering high temperature (60°C 99 -70° C) fluids injected in the ground by energy storage systems a potential environmental 100 impact has therefore to be considered. 101

Classic thermal tests or monitoring strategies often rely on local and point-based 102 measurements to monitor changes in temperature. In this context, geophysics can bring 103 complementary information which is spatially distributed and acquired directly from the ground 104 surface. In particular, electrical resistivity measurements could be considered as a time and 105 cost-efficient method for monitoring shallow geothermal systems to understand thermal 106 processes. Hermans et al. (2015) demonstrated the ability of cross-borehole time-lapse 107 resistivity tomography to study heat flow and heat storage within a small field experiment in a 108 shallow aquifer and Hermans et al. (2012) successfully used surface resistivity measurements 109 to monitor temperature variations. Fragkogiannis et al. (2008) also used resistivity tomography 110 for monitoring the thermal performance of an installed ground source heat pump system. Robert 111 et al. (2013), under laboratory conditions, highlighted the problems of resistivity-derived 112 temperatures owing to chemical reactions occurring both on fluid and solid phases. They 113 observed a divergence between resistivity and temperature curves, related to decreasing 114 solubility of some minerals (e.g. calcite precipitation) and resulting decreasing fluid 115 conductivity with increasing temperature. A more detailed review on the use of geophysical 116 methods to monitor temperature changes induced in the underground by shallow geothermal 117 systems can be found in Hermans et al. (2014). More case studies are also provided by Arato et 118 al. (2015). 119

Resistivity based measurements are potentially very powerful since useful relationships 120 can be found in literature between temperature and electrical resistivity (Campbell, 1948; Lee 121 and Deming, 1998; Fragkogiannis et al., 2008; Rein et al., 2004; Hayashi, 2004; Hayley et al., 122 2007). However, resistivity depends also in a complex way on different soil and environmental 123 attributes. Friedman (2005) gave an overview of these parameters, and their impact, underlining 124 three categories: (i) parameters describing the bulk soil, such as porosity (Φ), water content (θ) 125 and structure; (ii) the time-invariable solid particle quantifiers, such as particle shape and 126 orientation, particle-size distribution, wettability or cation exchange capacity; (iii) fast-127 changing environmental factors, such as ionic strength, cation composition and, finally, 128 temperature. A proper, but not easy, parameter calibration should be undertaken in order to 129 infer relevant information such as the extension of TAZ. Devoted tests are therefore necessary 130 in this respect. As an example, laboratory tests have the advantage that controlled boundary 131 conditions can be obtained (parameters from the first and the second groups) such that a direct 132 comparison of geophysical results, temperature measurements and numerical simulations can 133 be performed. After a proper calibration it will be then possible to use electric resistivity 134 variations with time as an imaging tool for the distribution of thermal plumes. This approach 135 can be also profitably extended at the field scale, if some of the mentioned parameters do not 136 change during time (particle size distribution, water content, porosity etc.). 137

The present paper therefore presents a series of laboratory tests performed on an *ad hoc* 138 designed apparatus for testing and calibrating a methodology for monitoring the extension of 139 TAZ caused by underground storage applications. A heat injection was induced in a porous 140 medium and time-lapse electrical measurements were carried out together with local 141 temperature measurements and a Finite Element Method (FEM) numerical simulation of the 142 heat propagation. Several tests were performed by varying: porous medium, position and 143 number of heat sources, hydraulic conditions and injection time. Resistivity and temperature 144 measurements were then compared with numerical simulations to estimate the reliability of 145 apparent resistivity variations in qualitatively mapping TAZ extension within the medium and 146 in quantitatively evaluating temperature distribution within it. 147

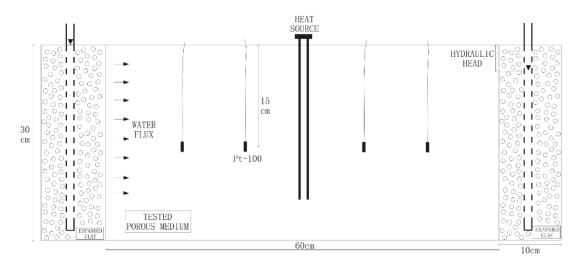
149 2. MATERIALS AND METHODS

- 150 The proposed testing methodology consists of the following steps:
- Analogical test: heat injection and heat turnoff monitored by 4 temperature sensors
 located in the medium and by hourly electrical measurements in spatial arrangement,
 on two different media;
- Numerical simulations: numerical modeling of heat propagation calibrated on local
 temperature measurements to extend temperature information spatially end evaluate the
 eventual differences in homogeneous parameters variation;
- Resistivity data processing: calibration of the fractional change in electrical resistivity
 based on the comparison with local resistivity data and temperature measurements;
- Temperature prediction and comparison: imaging of the resistivity-derived temperature
 maps by means of the previous step and comparison with the numerical simulations.

161 Details on the instrumentation and procedures adopted in each step are provided in the 162 following.

163 **2.1 Laboratory apparatus and performed tests**

A plastic box, sized 0.8 x 0.3 x 0.3 m (Fig. 1), was prepared to simulate a heat injection 164 within the selected porous medium. Three sectors separated by permeable septa were 165 predisposed in order to focus the simulation in the central part of the box. In the external sectors 166 two PVC pipes, surrounded by a high porosity filling material, were placed for generating a 167 water flux by controlling the hydraulic head in the pipes. The central sector, about 0.6 m long, 168 was filled with a porous medium for 0.3 m of thickness and was equipped with 4 thermo-169 resistances Pt100 (accuracy \pm 1°C, resolution 0.2°C), located at different positions depending 170 on the test, for the temperature monitoring. An electrical resistance (diameter 4 cm) and 171 powered by alternated current was used as heat source. During the tests, the source was 172 controlled by a thermometer and a rheostat, to assure desired constant temperature (60°C for 173 all the tests). For one of the presented tests a double source has been used (Tab. 1). The 174 boundaries of the box where thermally insulated using cork panels and impermeable 175 membranes. A data-logger and appropriate software were used for data acquisition, in order to 176 register continuously all the controlling parameters (sampling interval 1 minute). 177



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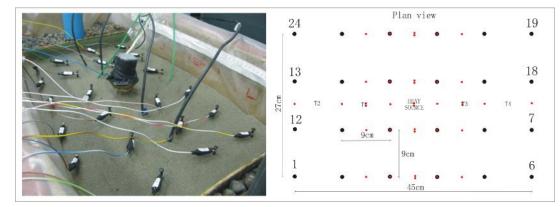
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Fig. 1. Schematic depiction of the laboratory device used for the experimental tests.

Tab. 1 – Summary of the presented tests

| Name | Porous medium | Water flux [l s ⁻¹] | Processes | Heat injection | Source position | | |
|------|------------------|------------------------------------|-------------------------|-------------------|---------------------------|--|--|
| Fs | Fine | - | Conduction | 9 h | 1 source central position | | |
| Fd | Fine | 1.5x10 ⁻³ | Conduction & convection | 5 h | 1 source central position | | |
| Cs | Coarse | - | Conduction | 5 h | 2 sources left side | | |
| Cd | Coarse | Coarse 3.0x10 ⁻³ | | 5 h | 1 source central position | | |

A network configuration with 24 electrodes (6 lines of 9 cm spaced electrodes) was 183 adopted to achieve a wide spatial information around the sources (Fig. 2). A SYSCAL Pro 184 multichannel georesistivimeter was used for resistivity measurements. A short current injection 185 time (250 ms) was adopted in order to record the set of measurements as quick as possible. A 186 dipole - dipole array with 36 measurements (plus reciprocal, for a total of 72 measurements) 187 was adopted. This configuration allowed us to record resistivity values roughly at the same 188 depth of temperature sensors and to image its variation during time in a plan view around the 189 heat source. Dipole - dipole configuration was adopted in order to improve data coverage, since 190 number of electrodes and available space are reduced. This situation often affects also real site 191 data, particularly in urban environment. Moreover, dipole - dipole is more prone to evaluate 192 lateral variation in resistivity as in the case for an advancing thermal plume. Midpoints of dipole 193 - dipole measurements are reported in red in Fig. 2. 194



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Fig. 2. Electrode configuration adopted in the tests with dipole-dipole centre location (red dots on the right); the picture and the position of the temperature sensors refer to Fs test.

Two natural porous media with different grain size distributions were adopted. These 198 materials come from two quarries nearby Torino and are therefore intended to represent typical 199 local geological conditions of the municipality. The two media were respectively made of: (i) 200 a fine medium with 91% wg. of sand and 9% wg. of silt, compacted at a porosity of 0.46; (ii) a 201 coarse medium with 58% wg. of gravel (mean particle diameter $d_0 = 5-6$ mm) and 42% wg. of 202 sand, compacted at a porosity of 0.35. In the present paper 4 examples of several tests conducted 203 in the box are presented (Tab. 1). The tests are intended to simulate the heat injection under 204 realistic conditions; in one of the tests a double injecting source was also used. In both media a 205 pure conduction test, with the medium completely saturated by tap water, and a conduction + 206 convection test, where a water flux was simulated by inducing a hydraulic head gap between 207 the two side of the box are presented. A flow rate of about 3.0 x 10^{-3} l/s of water at room 208 temperature was induced in the coarser medium, while the flow rate adopted in the finer was 209 about 1.5 x 10^{-3} l/s, owing to the different permeability coefficients of the tested media. The 210 tests lasted at least 10 hours, with 5 hours of heat injection and the remaining 5 hours of cool 211

down. The electrical surveys were performed hourly from the beginning (zero condition) until
the end of the tests, when the undisturbed temperature was reached again.

214 2.2 Numerical simulations

To simulate the heat injection within the medium, the OpenGeoSys code (OGS) was 215 adopted (Kolditz et al., 2012). OpenGeoSys is an open-source initiative for the numerical 216 simulation of thermo-hydro-mechanical/chemical processes. It is a flexible FEM numerical 217 framework, provided to solve multifield problems in porous and fractured media for several 218 geological and hydrological applications. The simulations were performed using the 219 heat_transport process for the static tests and the coupled heat_transport and 220 groundwater_flow processes for the tests simulating coupled conduction and forced convection 221 phenomena. The OGS governing equations for both "pure conduction" heat transport and 222 "conduction + convection" heat transport can be summarized in the energy balance equation, 223 taking into account every element of the bi-component medium (solid and water): 224 225

226

$$\gamma_b C_b \frac{\partial T}{\partial t} + \nabla \mathbf{q}_T = Q_T \tag{1}$$

where at the first member the temperature (*T*) variation as a function of time multiplied by density (γ_b) and specific heat capacity (C_b) of the medium are summed to the heat flux term q_T , which can be divided in the two components of advective and conductive flux as follows:

$$q_T = \Phi \theta \gamma_w C_w v T - \lambda_b \nabla T$$
^[2]

where Φ is the porosity, θ the water content, γ_w and C_w the density and the specific heat capacity of water, *v* denotes Darcy velocity and λ_b is the bulk thermal conductivity.

Some preliminary evaluations comparing *ad hoc* simulations with available analytical 233 solutions and experimental tests were used to calibrate geometric elements, discretization mesh, 234 Dirichlet and Neumann boundary conditions, time step definition, medium, material and fluid 235 properties. The simulations were carried out setting up the same characteristics of each 236 experimental test performed at lab scale. A 3D model with a rectangular prism mesh of about 237 75,000 nodes was adopted. Lateral sides of the box were simulated as impermeable boundaries, 238 not allowing for heat or fluid flow and only the upper boundary was a diffusing one. The finally 239 adopted physical properties of the tested materials are presented in **Tab. 2**. 240

241 242

Tab. 2 – Physical properties of the tested media adopted for numerical simulations.

| | . | γb | ki | λs | λw | Cs | Cw | Δi |
|------------------|----------|----------------------|---------------------|--------------------------------------|--------------------------------------|---------------------------------------|---------------------------------------|------|
| | Φ | [t m ⁻³] | [m ²] | [W m ⁻¹ K ⁻¹] | [W m ⁻¹ K ⁻¹] | [J kg ⁻¹ K ⁻¹] | [J kg ⁻¹ K ⁻¹] | [m] |
| Fine medium | 0.46 | 1.47 | 1x10 ⁻¹¹ | 5.0 | 0.58 | 800 | 4,200 | 0.05 |
| Coarse medium | 0.35 | 1.72 | 3x10 ⁻¹¹ | 5.0 | 0.58 | 800 | 4,200 | 0.05 |

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245 **2.3 Electrical resistivity vs. temperature**

246 2.3.1 Adopted methodology

A linear dependence between temperature and electrical conductivity (σ – the inverse of resistivity) can be assumed in the temperature range in question (Hermans et al., 2012). Around 25 °C the following relation has been proposed:

250 $\frac{\sigma_T}{\sigma_{25}} = m(T - 25) + 1$ [3]

where σ_T is the electric conductivity of the porous medium at temperature T (°C) and m is the 251 fractional change in electrical conductivity (°C⁻¹). A range of 0.018 °C⁻¹ and 0.025 °C⁻¹ has 252 been found by several authors for *m* (Revil et al., 1998; Hayashi, 2004; Hayley et al., 2007; 253 Hermans et al., 2012) and it varies according to the type of fluid and sediments. Water and 254 surface conductivity effects can be separated in case of a silty or clayey medium, accounting 255 for different fractional changes, m^{f} for fluid and m^{s} for surface conductivity. According to Revil 256 and Linde (2006) the surface conductivity is related with the average particle diameter of the 257 medium as follows: 258

 $\sigma_S = \frac{6\Sigma_S}{d_0}$ [4]

where Σ_S is the specific surface conductivity (S) and d_0 is the mean particle diameter. If we 260reasonably assume the specific surface conductivity equal to 4.0×10^{-9} S (Bolève et al., 2007), 261 we obtain $\sigma_s = 1.6 \times 10^{-4}$ S/m and $\sigma_s = 9.6 \times 10^{-6}$ S/m respectively for the finer ($d_0 = 0.15$ mm) 262 and the coarser media ($d_0 = 2.5$ mm). By considering that the applied tap water conductivity is 263 5.0×10^{-2} S/m, we can thus neglect the surface conductivity effect in the performed tests and 264 assume the bulk electrical resistivity variation during the heat injection completely related to 265 the water contribution. At the same time the reduced testing time allows also assuming constant 266 values for ionic strength and cation composition. These assumptions hold for the clay-free 267 materials under study and for limited heating time and may not be completely applicable in the 268 presence of high concentrations of carbonates. 269

We have now to transform **Eq. [3]** for the purposes of this study, and so to obtain a relationship between temperature and apparent resistivity variation. By considering σ_{25} as the reference value at the initial conditions, σ_T the value at a defined step during the test and by transforming the equation in terms of apparent resistivity we thus obtain:

274 $\frac{\rho_{a_0}}{\rho_{a_t}} = m(T_t - T_0) + 1$ [5]

where ρ_{a0} is the apparent resistivity at zero condition (before the starting of the heat injection), ρ_{at} is the apparent resistivity measured at a defined step, T₀ and T_t are temperature at the respective time. From **Eq. [5]** we can obtain:

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$$\Delta \rho(\%) = \frac{100}{m\,\Delta T + 1} - 100$$
 [6]

which relates apparent resistivity variation in percentage $\Delta \rho_a(\%)$ from zero condition to the difference in temperature ΔT , always depending on the fractional change in resistivity which is medium-dependent. With **Eq. [6]** we are able to predict the variation in resistivity by knowing the increase or the decrease in temperature induced in the tested medium. Analogously, by inverting the proposed relation in terms of temperature it is also possible to predict the temperature distribution within the medium by performing time-lapse electrical resistivity measurements, **Eq. [7]**:

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$$T_t = \frac{1}{m} \left(\frac{100}{\Delta \rho_a(\%) + 100} - 1 \right) + T_0$$
[7]

In our approach, we used apparent resistivities avoiding data inversion for several motivations:

- given the almost homogeneous condition of the tested materials, measured apparent resistivities can be quite reasonably approximated to the true resistivity of the medium;
- it is well known that inversion can introduce unwanted artifacts that may bias the
 results and interpretation particularly on sparse data;
- the limited number of electrodes (space requirements) and the few measurements
 performed did not provide enough data to allow for a rigorous inversion;
- on a complementary side, few electrodes and short current injection time is
 necessary for an acquisition time comparable to the monitored phenomenon and
 it is the most common situation in real sites with limited space;
- last but not least, we wanted to test a fast and simple methodology that could be
 potentially applied on site for monitoring purposes, at least in favorable sites (i.e.
 characterized by nearly homogeneous conditions), avoiding too much data
 elaboration.

Apparent resistivities were obtained from measured resistances by adopting a standard 303 geometric factor (k) for dipole - dipole array over infinite homogeneous half-space. To ensure 304 the reliability of this operation if compared to the limited dimensions of the box, forward model 305 simulations were carried out with R3t code (Prof. Andrew Binley, © 2012, Lancaster 306 University), considering the presence of insulating boundaries, in order to estimate k factor's 307 differences with respect to homogeneous half-space. Changes in geometrical factor greater than 308 15% were observed only close to the boarders of the box, while divergences in the center are 309 less than 10% and comparable to measurements' errors (see after). It has moreover to be 310 considered that data processing was performed with time-lapse differences with respect to 311 starting conditions; this procedure helps to eliminate the influence of the box's walls on the 312 apparent resistivity changes observed, being constant the effect on electric current paths during 313 the tests. 314

316 2.3.2 Data error analysis

As before mentioned, both normal and reciprocal resistance measurements were acquired. Together with repeatability tests, reciprocal error quantification can be adopted as a measure of noise in order to prevent misinterpretation of ERT images (Slater et al., 2000). In the present study, repeatability tests were not performed because as fast as possible resistivity measurements were needed. Only reciprocal errors were quantified and analyzed in order to evaluate reliability of the measurements. Reciprocal error known as $E_{N/R}$ (LaBrecque et al., 1996) can be achieved by:

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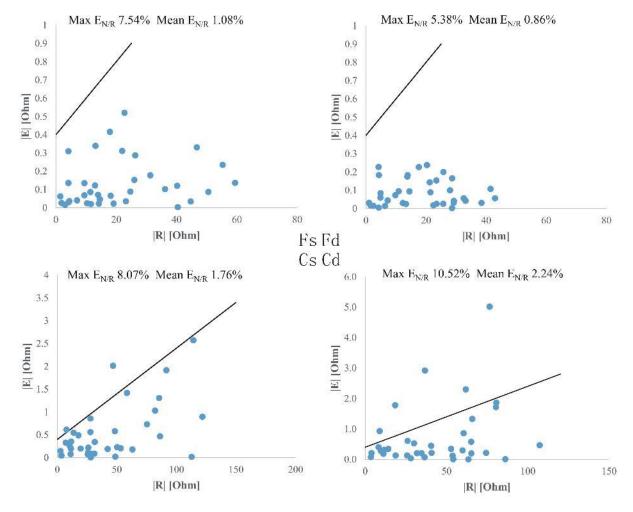
$$|E_{N/R}| = R_n - R_r \qquad \text{Eq. [8]}$$

where R_n and R_r are resistances measured by normal and reciprocal quadrupoles respectively. Since for the principle of reciprocity exchanging current and potential electrodes should not change measured resistance, reciprocal error gives a measure of data noise.

 $E_{N/R}$ of each measurement step during heat injection tests were plotted against resistance data *R* (average between normal and reciprocal) and an error envelope given by:

 $|E_{N/R}| = a + b \cdot |R|$ Eq. [9]

with a = 0.4 and b = 0.02, encompassed almost the totality of data in each test. As showed in 331 Fig. 3, Cd is the worst test, with 6-7 outliers but only 1 of them with error greater than 10%, 332 which is typically adopted as threshold (Slater et al., 2000). We therefore decided to keep all 333 data sets in each experiment here presented, because even if erasing outliers could bring to 334 better apparent resistivity estimation, it is however true that an artificial kriging interpolation 335 obtained by voids in the measurements can bring to exaggerated smoothing or artificial imaging 336 in the 2D maps. In this case, where only few measurement points are available (owing to above 337 mentioned reasons), it was decided to keep all the data but being aware of reciprocal error 338 distribution during data interpretation. Again, working with time-lapse differences can lower 339 the influence of this error on data processing; indeed, in the performed evaluations $E_{N/R}$ was 340 observed to remain almost constant during the whole duration of the tests. 341





343Fig. 3. Reciprocal error |E| plotted against average resistance values |R| for the zero condition (before heat344injection started) of each test. Black lines are the error envelope with a = 0.4 and b = 0.02. Maximum and mean345reciprocal errors of each test are also reported.

347 3. RESULTS

The results of the numerical simulations in each of the 4 tests compared with the 348 temperature experimental data are reported in Fig. 4 (for reference to the location of 349 temperature sensors refer to Figs. 6-9). In Tab. 3, the misfit of numerical versus experimental 350 temperatures are reported. It can be observed that a valid match was reached in most of the tests 351 allowing for the reconstruction of the full temperature field inside the box. Particularly the 352 average misfit values remained below 3.5 % for all the tests apart the one under static water 353 condition on the fine material (Fs test) which indeed show an increased average uncertainty. 354 This test is also the one having the longer injection time causing possible evaporation 355 phenomena as will be discussed in section 4. 356

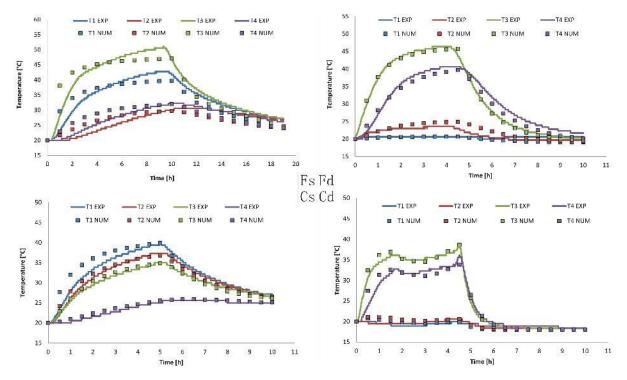
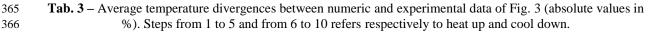


Fig. 4. Comparison between measured (continuous curves) and numerical (dotted curves) temperature data in all the tests. In the Fs test, T2 and T1 were 15 and 8 cm upline of the source, while T3 and T4 were downstream at 5 and 15 cm respectively. For the Fd and Cd tests T1, T2 and T3 were placed at about 10 cm around the source, while T4 was at 20 cm. In the Cs test T1, T2 and T3 were placed at 8 from one of the sources, while T4 was at 20 cm; the OGS numerical simulation also managed to represent the unwanted temperature decrease at the source during the Cd test.



| Test | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | Average |
|------|-------|------|------|------|------|------|------|------|------|------|---------|
| Fs | 13.06 | 7.65 | 4.96 | 4.55 | 1.84 | 7.63 | 9.02 | 8.84 | 9.44 | 9.90 | 7.69 |
| Fd | 1.61 | 1.86 | 1.96 | 2.59 | 4.36 | 4.39 | 4.88 | 4.05 | 4.68 | 5.47 | 3.59 |
| Cs | 6.33 | 4.22 | 3.41 | 1.63 | 1.02 | 2.37 | 2.42 | 3.13 | 2.50 | 1.47 | 2.85 |
| Cd | 6.26 | 2.86 | 3.47 | 1.38 | 3.53 | 2.73 | 3.10 | 2.71 | 2.07 | 2.10 | 3.02 |

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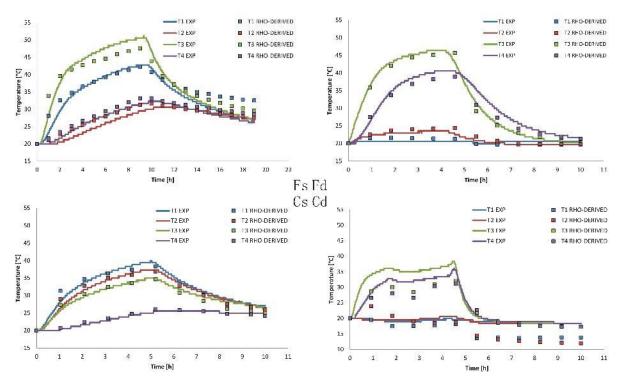
The flowing water test on the coarse material (Cd test) showed the smallest peak temperature because of the high velocity of the induced flux, which did not allow the water to

heat up the medium properly. Contrary to the other ones this test do not present big variations 370 between the first and the last hour of the heating period. The hydraulic flux warmed up the 371 medium more rapidly, reaching the temperature peak within the first hour. Moreover, after the 372 peak, an unexpected temperature decrease in the heat injection during the test (from 60 °C to 373 50 °C from hour 1.5 to hour 3) was recorded. This effect was taken into account in the 374 simulations. The analogous test in the fine medium is instead characterized by curves shaped 375 similarly to stationary tests (Fs and Cs) due to the slower flow velocity. The flux velocity plays 376 therefore a major role in transporting the heat. Among all the tests, those performed in the fine 377 medium reached the biggest temperature peaks. A finer material is more able to limit the heat 378 losses than a coarser one. These losses are mainly ascribable to the pore-filling water, which is 379 obviously less constrained by the capillary pressure in a coarser than in a finer medium. 380

Fig. 5 shows the comparison between the temperature recorded by the 4 sensors during 381 the tests (for reference in the location of temperature sensors refer to Figs. 6-9) and the 382 resistivity-derived temperature obtained by applying Eq. [7] to the local resistivity 383 measurements nearby the sensors. Best fit m values of 0.025 $^{\circ}C^{-1}$, for the finer medium, and of 384 0.021 °C⁻¹, for the coarser medium were obtained, reaching again a valid match both in static 385 and in dynamic conditions. The temperature-sensitivity of resistivity data is particularly clear 386 in the test on the coarse material (Cd test): resistivity data are indeed able to reflect the 387 temperature trend during heating related to the decrease in temperature of the source. In the 388 cooling periods a divergence between temperature and resistivity-derived data is highlighted in 389 Fs and Cd tests. In the first case the resistivity-derived temperature shows a slower return to the 390 initial conditions with respect to T-sensor recordings, in the second case the opposite is true. In 391 Tab. 4 the misfit of resistivity-derived versus experimental temperatures are reported. A valid 392 agreement can be particularly noted in all the heating periods with an average misfit below 5%. 393 In Fs and Cd tests an increase in the average misfit (particularly high for the Cd test) is observed. 394 Motivations for this divergence will be discussed in Section 4. 395

| Test | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | Average |
|------|-------|-------|-------|-------|-------|-------|-------|-------|-------|-------|---------|
| Fs | 7.62 | 4.96 | 4.41 | 4.52 | 4.05 | 1.62 | 4.62 | 6.47 | 8.40 | 9.36 | 5.60 |
| Fd | 3.30 | 3.46 | 3.64 | 3.43 | 5.33 | 7.13 | 3.61 | 2.77 | 3.10 | 2.84 | 3.86 |
| Cs | 5.74 | 2.58 | 1.59 | 1.21 | 1.61 | 2.24 | 2.21 | 4.85 | 3.26 | 4.91 | 3.02 |
| Cd | 11.05 | 13.15 | 13.26 | 11.01 | 11.35 | 20.49 | 20.07 | 23.34 | 23.75 | 24.60 | 17.21 |

Tab. 4 – Average temperature divergences between resistivity-derived and experimental data of Fig. 4 (absolute values in %). Steps from 1 to 5 and from 6 to 10 refers respectively to heat up and cool down.



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Fig. 5. Comparison between measured (continuous curves) and resistivity-derived (dotted curves) temperature
 data in all the tests. The latter are calculated with Eq. [7] from the resistivity data registered by quadrupoles just
 around the sensors.

Finally, Figs. 6, 7, 8 and 9 present the comparison between numerically modelled and 403 resistivity-derived temperatures in all the tests in a 2D representation. These maps were 404 obtained with a Kriging interpolation of the temperature values deduced by apparent resistivity 405 variation. Kriging method was applied accounting for the analysis of the spatial data variability; 406 in each test, best fit of experimental variograms was found to be a linear variogram model in 407 every time step. Apparent resistivity monitoring highlighted its potentiality in describing the 408 heat diffusion from the source in all the tests. In the Fs test (Fig. 6), which is the longest among 409 all the performed tests, temperature maps near the peak are not so homogeneous and also the 410 cooling down shows some portions where the resistivity is higher (white portions above and 411 below the source) and other parts where instead a lower resistivity generated a higher 412 temperature estimation. The experiment with flowing water in the fine medium (Fd, Fig. 7) 413 shows a good agreement throughout the whole testing time. The left portion of the maps 414 remained at an almost constant temperature for the entire heating period, while the right portion 415 is validly described by the resistivity monitoring, except for some heterogeneities just around 416 the source. The Cs is the best example among all (Fig. 8): the heating period is in valid 417 accordance with the peak temperatures and the shape of the heated plume (caused by the 418 presence of two heating sources); the cooling down is also correctly described by the resistivity 419 monitoring. The flowing water test on the coarse material (Cd, Fig. 9) shows the ability of the 420 electrical surveys to qualitatively describe the migration of the heated plume due to the water 421 flux. The heating predominant in the right portion of the box is clearly highlighted. The 422 423 quantitative representation of the temperature field is however not effective as already commented in relation to Fig. 5. The discrepancy of the resistivity derived maps from the 424 homogeneous reference condition of numerical simulations (particularly Figs. 6 and 9) is 425 however not surprising since probable different effects could be present. Again, motivations for 426 the evidenced discrepancies will be commented in Section 4. 427

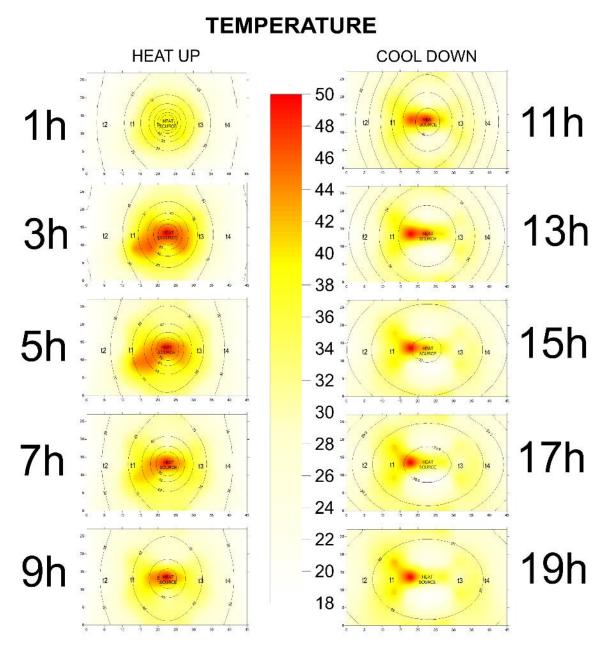


Fig. 6. Comparison between numerical (contours) and resistivity-derived (colored maps) temperature data in the
 Fs test. The numerical temperature is provided by the OGS simulation calibrated on the temperature recorded by
 each sensor. The resistivity-derived temperature is obtained by Kriging local resistivity transformed data.

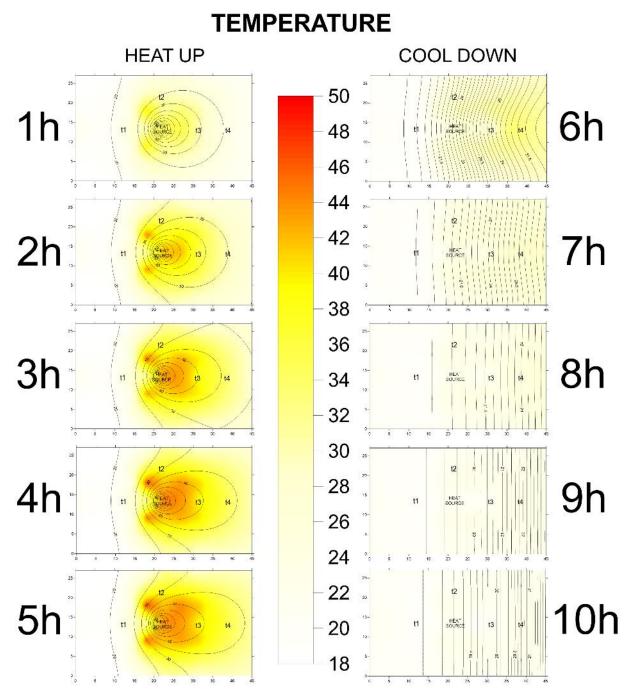
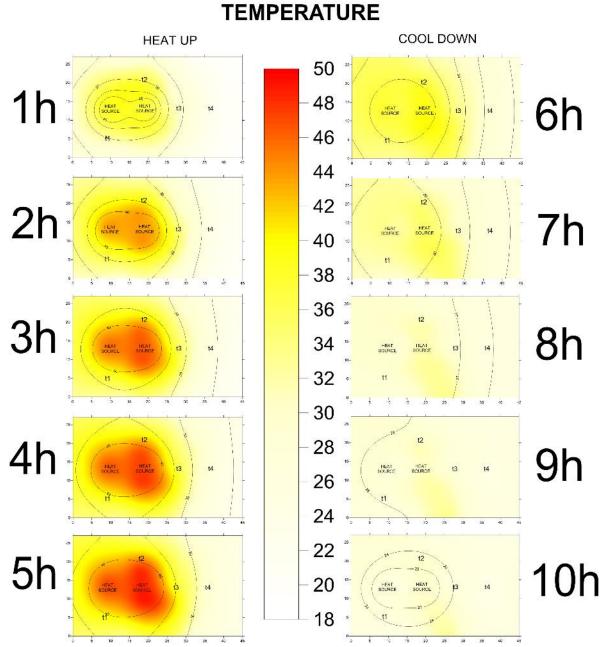
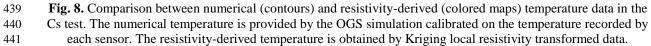
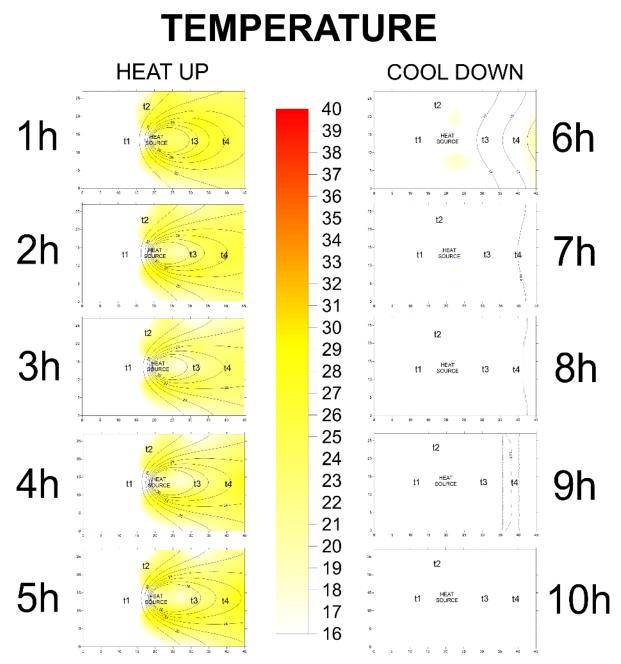


Fig. 7. Comparison between numerical (contours) and resistivity-derived (colored maps) temperature data in the
 Fd test. The numerical temperature is provided by the OGS simulation calibrated on the temperature recorded by
 each sensor. The resistivity-derived temperature is obtained by Kriging local resistivity transformed data.







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Fig. 9. Comparison between numerical (contours) and resistivity-derived (colored maps) temperature data in the
 Cd test. The numerical temperature is provided by the OGS simulation calibrated on the temperature recorded by
 each sensor. The resistivity-derived temperature is obtained by Kriging local resistivity transformed data.

For quantitatively evaluate the fit of the resistivity estimated temperatures, each 447 resistivity-derived temperature map was compared with the numerical one at each time step. 448 The average of the divergences for each time step is reported in Tab. 5. Generally an 449 overestimation trend was always observed. Fs, Fd and Cs tests stand at an acceptable bias of 10 450 \pm 2%, while Cd shows worse values, as expected. Among all the tests, in the Cs experiment the 451 best agreement was found, confirming the effective temperature estimate shown in the above 452 reported figures. Conversely to the others, the Cs bias decreases when approaching the peak of 453 the heat injection, reaching the smallest value 1 h after the source's turning off. Fig. 10 reports 454 a comparison between the numerical and the resistivity-derived TAZ. This can better help in 455 evaluating the potentiality of the resistivity monitoring for imaging the extension of the thermal 456 plume. Fs, Fd and Cs show a valid agreement with a little overestimation particularly in the 457 higher isotherm (40°C). Cd test is clearly more disturbed than the others. In general, it can be 458

said that the resistivity measurements performed during the heat injection described the TAZ
 induced in the medium with an acceptable misfit and that the little overestimation of their
 extension can be seen as conservative.

462 Tab. 5 – Average temperature divergences between numeric and resistivity-derived data of Figs from 5 to 8
 463 (absolute value in %). Steps from 1 to 5 and from 6 to 10 refers respectively to heat up and cool down.

| Test | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | Average |
|------|-------|-------|-------|-------|-------|-------|-------|-------|-------|-------|---------|
| Fs | 9.86 | 11.16 | 12.10 | 14.78 | 13.87 | 10.42 | 11.20 | 12.21 | 13.41 | 14.80 | 12.38 |
| Fd | 10.78 | 11.56 | 11.71 | 11.86 | 12.40 | 7.14 | 6.84 | 6.61 | 7.93 | 7.79 | 9.46 |
| Cs | 10.09 | 7.61 | 7.27 | 7.13 | 7.32 | 6.14 | 6.29 | 6.59 | 8.94 | 12.64 | 8.00 |
| Cd | 25.23 | 26.01 | 28.05 | 29.43 | 29.78 | 28.04 | 37.89 | 39.78 | 41.03 | 41.54 | 32.68 |

464

465 **4. DISCUSSION**

The numerical modeling was useful to obtain a reference temperature distribution within the medium. The 4 time-lapse local temperature curves registered by the sensors were not sufficient alone to interpolate the induced thermal plume throughout the medium This is a common problem when local temperature monitoring points are adopted.

From a first qualitative look, the results of the electrical surveys showed the expected 470 correlation of decreasing electrical resistivity with the increasing temperature induced by the 471 heat injection, the opposite is true after the source's turning off. The electrical resistivity 472 changed more slowly with increasing distance from the heat source, as temperature did, and 473 resulted dependent upon the water flux conditions within the material. As an average between 474 all the performed tests (both fine and coarse medium), it was observed that a 10% positive 475 variation in temperature generates a 2% - 3% negative change in electrical resistivity. 476 Generally, the heating periods were appreciably monitored by resistivity measurements and the 477 resistivity-derived temperatures are in valid accordance with the numerical model. Conversely, 478 in the cooling periods a slight divergence between temperature and resistivity-derived data is 479 particularly highlighted in Fs and Cd tests (Fig. 5), same divergences are also partially noticed 480 in the comparison of temperature and numerical curves (Fig. 4). At the same time some 481 heterogeneities appears in some of the presented resistivity-derived temperature maps 482 (particularly in Fs and Cd tests, Fig. 6 and 9). These can be related to different phenomena 483 occurring in the medium: (i) evaporation, (ii) chemical reactions induced in the water and (iii) 484 velocity of the water flux. 485

Evaporation process seems to disturb only when a prolonged heat injection is performed. (i) 486 The resistivity measurements were indeed mainly disturbed in the Fs test, in which a 9 h 487 heat injection was performed, while they were not influenced in other experiments. 488 Evaporation processes, observed on the surface of the box, caused a fictitious increase in 489 resistivity which is not related to the temperature dependence, so that heterogeneities may 490 occur in temperature visualization (Fig. 6) and anomalies in the resistivity derived 491 temperature curves (Fig. 5). The evaporation process has been quantified by local direct 492 measurements at the end of the test showing a reduction of about 10% water content in a 493 10 cm zone around the source. This reflect in a more remarkable temperature difference 494 for the sensors located near the source (T1 and T3) than for the farthest ones (T2 and T4). 495 Since the temperature estimation from resistivity data is based on a measured resistivity 496 difference this effect could cause both a lower estimated temperature at the peak and an 497 higher estimated temperature in cool down. 498

(ii) During the cool down of the same test, data show a return to slightly lower resistivity in 499 respect to the initial condition (higher apparent temperature). This can be attributed to 500 chemical reactions' effect (e.g. mineral dissolution processes occurred in the medium 501 during the heating up). We can hypothesize that the heat injection produces an increase 502 in water TDS (total dissolved solids) that lowers the bulk medium resistivity. As for 503 evaporation, chemical reactions' problem only occurs when a prolonged heat injection is 504 performed; no bias related to this issue is highlighted in other tests. A quantification of 505 this effect was indeed performed during the Fs and Fd tests by measuring fluid resistivity. 506 In Fs test, a value of $22.3 \pm 0.1 \Omega$ m was measured in the water squeezed from a sample 507 at the end of the test. Conversely, in the Fd test a value of $22.8 \pm 0.1 \Omega$ m was constantly 508 monitored in the water going out of the box after passing through the medium. The initial 509 water resistivity was 22.7 Ω m in both tests. This means that during the conduction + 510 convection test (Fd) no relevant water resistivity variation due to changes in TDS was 511 observed, while an only slight reduction was noted in the pure conduction test (Fs) 512 partially responsible, together with evaporation, of worse data fit. It must be also 513 underlined that the above mentioned water resistivity values were estimated on the whole 514 water volume within the box, smearing possible localized anomalies. It is thus possible 515 that, in limited zones nearby the source, mineral dissolution effect could be more relevant. 516 Generally, we can however say that more specific analyses are necessary in order to 517 evaluate and discern evaporation and chemical reactions influences on resistivity 518 measurements. Divergences here highlighted between registered and resistivity-derived 519 temperatures can be of course related to the action of both processes together. 520

Flux velocity, higher in the Cd test, provided worse resistivity-derived temperatures (Fig. 521 (iii) 5). The rapid change of the flowing water within the box did not allow the heat injection 522 to change the water resistivity in the medium's portions located upstream of the source. 523 Moreover, a slightly higher resistivity is observed after source's turning off, showing a 524 cool down due to the lower temperature of the water flow. The difference of the 2D 525 temperature maps (numerical and resistivity-derived) in this test (Fig. 10) also underlines 526 that localized flow paths could be present in the coarser material. These are not reflected 527 in the numerical simulation, which assumes an homogeneous medium, but they are 528 underlined in the resistivity measurements. In the Fd test, in which the flux is slower, heat 529 injection is able to change water resistivity, so the two results are in better agreement. It 530 can be said that resistivity-derived temperature are reliable in the dynamic test with low 531 flux velocity, while they are less trustworthy when a high flux velocity is provided. 532

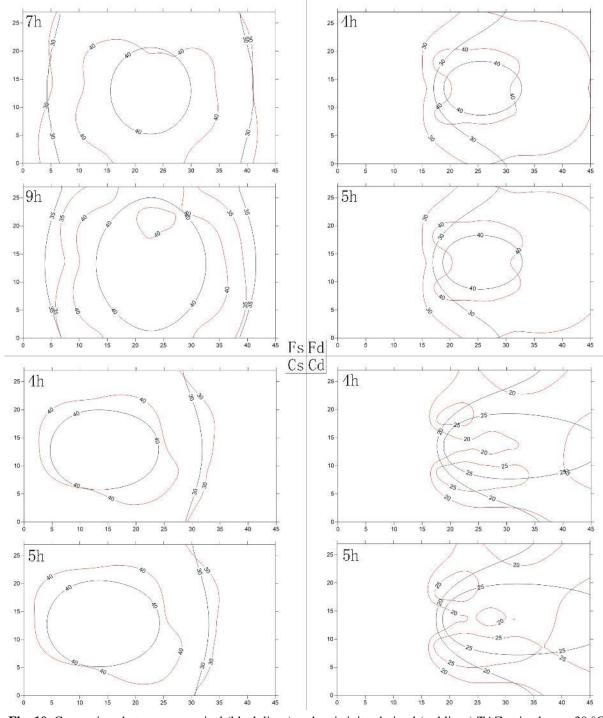


Fig. 10. Comparison between numerical (black lines) and resistivity-derived (red lines) TAZ at isotherms 30 °C
 and 40 °C for Fs, Fd and Cs; for Cd, isotherms 20 °C and 25 °C were adopted. For all the tests, two steps close to
 the heating peak are showed.

538 4. CONCLUSIONS

The present paper presented a series of tests carried out on a laboratory device, build for testing and calibrating the use of electrical apparent resistivity measurements for monitoring the thermal affected zone caused by heat injection. Four examples among the several performed tests were presented. Hourly apparent resistivity measurements were performed on two different porous media in order to image the temperature field within the box. The methodology was supported by numerical simulations calibrated on the temperature recorded by the sensors.

The outcomes of the tests highlighted the reliability of the time-lapse electrical 545 measurements for qualitatively predicting the heat propagation within saturated porous media. 546 The tests showed an acceptable agreement between the TAZ extensions extracted from different 547 approaches (e.g. direct temperature measurements, numerical simulations and apparent 548 resistivity measurements). Radial heat diffusion from the heat source was well described by the 549 variation of apparent resistivity data in tests without flowing water. Tests under flowing water 550 conditions underlined the disturbance of the water flux on the electrical resistivity 551 measurements; the faster the flux velocity, the higher the interference in the collected data. 552 Resistivity measurements appears to reveal more details then simple thermal or thermo-553 hydraulic modeling. Further studies are however necessary for completely understanding the 554 eventual influence of chemical reactions which occur in a porous medium when a heat injection 555 is provided, particularly at laboratory scale. This could provide a better calibration of resistivity-556 derived curves in order to be applicable also in field testing. 557

This study was precursor to what we are planning to do on a living lab prepared at the campus of Torino University in Grugliasco (Giordano et al., 2016; GTES, 2014), where a small ground heat storage system was built. The purpose of this living lab is to replicate at the field scale the laboratory experiments here presented and to serve as a model for further concrete developments of energy saving applications in northern Italy.

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