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A review of magnetic separation of whey proteins and potential application to whey proteins recovery, isolation and utilization.

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## 27 1.Introduction

28 Dairy products industry plays an important role in economic activity in many emerging  
29 and developed countries. For instance, in 2016 nearly 10 billion liters of milk were produced in  
30 Argentina (“Agroindustria.gob.ar,” n.d.). Over 40 percent of the total milk production is  
31 destined to cheese elaboration (Paez et al., n.d.). From this process, cheese whey (CW) emerges  
32 as a voluminous effluent constituted by proteins, lactose, vitamins and mineral salts. Around 0.9  
33 L of whey are generated per L of milk. A considerable fraction of lactose and milk proteins  
34 remain solubilized after precipitation by rennet or acids. CW is a large reserve of dietary  
35 proteins that remains outside the channels of human consumption when reutilization or  
36 revalorization procedures are not implemented. It is a substance of high nutritional value, but  
37 very polluting on contact with natural water and expensive to process. The limited management  
38 of CW brings a high indirect environmental problem. As a matter of fact, many researchers  
39 point out how polluting raw whey is due to its large biochemical and chemical oxygen demand  
40 impact. Efforts are made to clean the whey and enable its safe discarding (Ganju and Gogate,  
41 2017; Remón et al., 2016; Yadav et al., 2015) and to include the proteins in cheese, as one of  
42 the viable options to decrease the impact (Masotti et al., 2017).

43 The current treatments are almost restricted to the use of membrane technologies,  
44 i.e. ultrafiltration, nanofiltration, microfiltration and inverse osmosis. From these procedures  
45 products as whey powder, demineralized whey powder, permeate powder, food grade lactose  
46 and WPC (whey protein concentrate) can be obtained in Argentina. Protein powders are  
47 considered to provide high quality protein that may be quickly available to enhance post-  
48 exercise recovery (Hogan et al., 2016). These alternatives are feasible for companies that are  
49 able to process large volumes of whey and have an important investment capacity. As a result,  
50 the valorisation of CW is a limiting issue for small and medium businesses. The conversion of  
51 the whey into a valuable and exportable product means a positive economic impact, the  
52 preservation of the environment (as it industrializes a residue of cheese processing) and a  
53 contribution to regional and national development. In this context, magnetic nanotechnology  
54 emerges as a valuable tool for the recovery of protein based on the magnetic separation  
55 principle. A special interest is focused on magnetic nanoparticles based on iron oxide  
56 magnetite/maghemite with a functionalizing coating able to bind specific molecules (Mehta,  
57 2017).

58 MNPs have been thoroughly studied for biomolecules separation; however, their  
59 specific application to CW proteins isolation and purification has been barely reported.  
60 Combination or even substitution of filtration membrane technology by magnetic separation  
61 would be not only cost-effective but also would simplify whey process design. In this  
62 contribution, isolation of proteins from milk, whey or model systems is reviewed, focusing on  
63 magnetic supports, and more specifically in magnetic nanomaterials as materials to assess the  
64 recovery. The purpose is to gain insight into the feasibility of whey proteins separation and  
65 purification providing value to an extensive residue derived from one of the most important  
66 industries in Argentina. Besides the procedures proposed here, involving the magnetic  
67 nanomaterials may be useful in any milk-producing country and could be extrapolated to other  
68 milk-based food residues.

## 69 2. Generalities on cheese whey: Composition and available treatments

70 The products derived from CW are combination of diverse nutrients. Each bovine protein  
71 possesses *separately* interesting functionalities that require a high degree of purification.  
72 Lactoferrin,  $\beta$ -lactoglobulin,  $\alpha$ -lactalbumin, immunoglobulins, lactoperoxidase and bovine  
73 serum albumin (BSA) are all of interest. Lysozyme is also present in cheese whey although in  
74 extremely low concentrations ( $< 1$  mg/L) (Vasavada and Cousin, 1993). Practically all  
75 publications dealing with the characterization of cheese whey include detailed information  
76 about physicochemical properties of each protein (such as molecular structure, weight or  
77 isoelectric point). Hence, it will not be repeated here because of the different focus proposed for

78 this manuscript (Kinsella and Whitehead, 1989; Yadav et al., 2015). A brief description of the  
79 most relevant proteins is presented as follows:

- 80 ➤ Lactoferrin has shown anti-microbial and anti-viral activity (Embleton et al., 2013;  
81 Wakabayashi et al., 2014), anti-cancer properties (Lim et al., 2015; Song et al., 2017),  
82 tissue regeneration capacity (Shi et al., 2017) and other important functions (García-  
83 Montoya et al., 2012).
- 84 ➤ Purified  $\beta$ -lactoglobulin can be used for the detection of cow milk protein intolerance  
85 (Aich et al., 2015). A concrete function of this milk protein is not yet found, however it is  
86 capable of binding to hydrophobic ligands like cholesterol and vitamin D2 (Hochwallner  
87 et al., 2014).
- 88 ➤  $\alpha$ -Lactalbumin is appreciated as a source of peptides with numerous bioactivities such  
89 as anti-cancer, which may be utilized in the production of functional foods (Kamau et al.,  
90 2010). Bovine immunoglobulins improve symptoms, nutritional status, and various  
91 biomarkers associated with intestinal pathologies (Petschow et al., 2014).
- 92 ➤ Lactoperoxidase is a natural enzyme of the mammals' host defense system carrying  
93 antimicrobial and antiviral properties (Madureira et al., 2007).
- 94 ➤ BSA has been historically used as a protein concentration standard and *in vitro*  
95 biochemical assays.

96 The most efficient separation and purification techniques available for CW protein  
97 extraction are filtration membranes (Ganju and Gogate, 2017; Saxena et al., 2009) and  
98 chromatography (in column or membranes) (Chase and El-sayed, 2011). Variable pore sizes are  
99 then employed depending on the required selectivity. Membrane processes are volume-  
100 dependent separation methods, wherein the equipment capacity and cost of manufacture is  
101 proportional to the volume of solution processed and not to the mass of product. Filtration using  
102 membranes occurs by allowing molecules of certain size to pass through and excluding others.

103 Organic polymer membranes are the leading type for industrial applications.  
104 Nevertheless, they are prone to chemical or bio-fouling (Mikhaylin and Bazinet, 2016;  
105 Steinhauer et al., 2015), low fluxes, low mechanical strength and restricted chemical and  
106 thermal stability (Ishak et al., 2017). Ceramic membranes are considered the best candidates to  
107 replace polymeric membranes. Due to the high amount of flux, separation efficiency, long  
108 lifetime, and a continuous decrease in fabrication costs, research on ceramic membranes is  
109 increasing fast (Qiu et al., 2017).

110 Chromatographic separation of proteins consists in their selective adsorption on a  
111 functionalized solid (packed column or a membrane) and subsequent elution with a liquid  
112 phase. The interaction between the biomolecule and the stationary phase may present a diverse  
113 nature: hydrophobic (Santos et al., 2011), ionic (Li et al., 2017), or other specific affinity like  
114 dye binding (Urtasun et al., 2017) or transition-metal binding (Li et al., 2008).

115 Packed-column chromatography steps are effective and specific in the enrichment of  
116 bioactive peptides within downstream processes. On the other hand, they are time-consuming  
117 when applied using conventional laboratory methods. These processes are expensive, difficult to  
118 apply and, in some cases, may affect the secondary structure of peptides, resulting in the  
119 possible alteration or elimination of their bioactive characteristics. In view of this, industrial  
120 scale-up is not economically viable for the food industry (Dullius et al., 2018).

121 In opposition to column-filling materials, MNPs offer the alternative of solid-liquid  
122 extraction in batch mode. The adsorbents with a magnetic core do not need to be packed into  
123 cartridges, and the centrifugation steps may be substituted by the magnetic decantation mediated  
124 by an external magnetic field to achieve solid-liquid separation (X. Ding et al., 2015). Another  
125 disadvantage of standard column liquid chromatography procedures is related to the  
126 impossibility of to cope with samples containing particulate or suspended material –like raw  
127 cheese whey– so they are not suitable for work in early stages of the isolation/purification  
128 process. In this case magnetically modified two-phase systems have shown their usefulness  
129 (Safarik and Safarikova, 2004).

130 Table 1 summarizes the current trends in whey protein fractionation and the  
 131 fundamentals of these techniques.  
 132

133 **Table 1.** Working principles of whey protein purification techniques (based on Chase and El-  
 134 sayed, 2011).  
 135

<b>Chromatography</b>		
<i>Ion exchange</i>	<i>Affinity</i>	<i>Unspecific adsorption</i>
Net charge-based interactions	Selective adsorption/ elution	-Hydrophobic interactions
-Anion exchange (Santos et al., 2012)	-Specific interactions between proteins and immobilized ligands like metals (Carvalho et al., 2014), dyes (Baieli et al., 2014), bio-affined molecules (Lai et al., 2013) and others.	(Conrado et al., 2005), other non-specified
-Cation exchange (Doulton et al., 2004)		
-Mixed ion exchange (Saufi and Fee, 2011)		
<b>Filtration membranes</b>		
Transversal or tangential flow. Size-based separation. Variable pore size membranes	-Electro separation	
-Ultrafiltration (Chamberland et al., 2017)	-Electrodialysis: for the elimination of ions. Selective migration of ions through a membrane under an electric field (Mikhaylin et al., 2018)	
-Microfiltration (Hernández and Harte, 2009)	-Electroacidification: bipolar membranes that dissociate water molecules at their interfaces (Bazinet et al., 2004)	
-Nanofiltration (Cohen et al., 2017)		
-Reverse osmosis (Yorgun et al., 2008)		

136

137 In practice, two or more techniques are combined in a deliberate order for whey  
 138 treatment. Scheme 1 represents examples for obtaining WPI (whey protein isolate) and WPC  
 139 (whey protein concentrate).

140 **Scheme 1.** Examples of WPC and WPI obtaining pathways.

141 As stated, these technologies demand a strong investment. Therefore, it is necessary to  
 142 develop alternative separation techniques affordable to local and small-scale producers. MNPs,  
 143 especially those based in magnetite ( $\text{Fe}_3\text{O}_4$ ) have been used for immobilization of molecules  
 144 including drugs (Hauser et al., 2015), enzymes (Netto et al., 2013), other proteins (Iype et al.,  
 145 2017), genes (Vosen et al., 2016), antibodies (Gu et al., 2016) and even whole cells (Chen et al.,  
 146 2016). MNPs have proven to be useful in the purification of proteins from their native medium  
 147 (Gädke et al., 2017). Actually, MNPs can be considered as a particular type of stationary phase  
 148 in liquid affinity chromatography. Simple batch systems are perfectly suitable for sample  
 149 treatment in small or large scale. Applying the appropriate elution conditions, the immobilized  
 150 species can be recovered in pure form, whereas the MNPs can be reused in several purification  
 151 cycles (Zhou et al., 2018).

152 **3. Magnetic nanomaterials useful for protein separation**

153 The structure of MNPs, independently of their use, consists generally in an inorganic  
 154 magnetic core (usually magnetite/maghemite) coated with a shell, of varied nature, i.e small  
 155 molecules (organic or inorganic) or polymeric moieties, depending on the desired applications.  
 156 Their preparation may be achieved through several methodologies. The simplest one is co-  
 157 precipitation of magnetite from  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$  salts by adding a base like NaOH in presence of a  
 158 surfactant or functional molecule under nitrogen atmosphere and magnetic stirring (Figure 1).  
 159 This particular technique makes MNPs a very low-cost material (Azcona et al., 2016; Nicolás et  
 160 al., 2014, 2013). Commercial magnetite is also available in the market at an accessible price. For  
 161 example 97 % purity magnetite nanopowder (Aldrich) costs 903 dollars/250 g. Materials like  
 162 Poly(N-isopropylacrylamide) cost 782 dollars/10 g, and a carboxymethyl-functionalized cation  
 163 exchanger is 1188 dollars/ 250 mL (Supelco). All this information is valid for Argentina in the  
 164 Sigma-Aldrich website. Scanning the prices of the traditional beads it is clear that market value  
 165 of iron oxide nanopowder is sensibly lower.

166  
 167  
 168 **Figure 1.** Reactor disposition for coprecipitation of MNPs.

169 Due to their nanosize (5-20 nm), MNPs have the particular property of superparamagnetism.  
 170 This behavior allows to direct the position of the particles with an external magnetic field and  
 171 additionally, no magnetization remains after removing such field (null remanence).  
 172 Hydrodynamic diameter (often measured by dynamic light scattering) may be significantly  
 173 larger than the one observed by electronic microscopy since the particles tend to aggregate. The  
 174 aggregation of the MNPs in a liquid medium is highly dependent on their surface charge. Zeta  
 175 potential ( $\zeta$ pot) is a good indicator of the stability of MNPs in suspension. Its sign and  
 176 magnitude may be adjustable by controlling the pH of the medium if the particles contain  
 177 protonated/deprotonated groups (Liu et al., 2018; Vega-Chacón et al., 2017).

178 The magnetic core is chemically modified in order to provide them with a selective affinity  
 179 towards the target protein. Normally the mechanisms operating to bind to the proteins are the  
 180 following:

- 181 -Mostly electrostatic, dependent on the surface charge of both the particle and the target molecule.  
 182 These charges are tunable by adjusting the pH of contact medium.
- 183 -Mostly hydrophobic, interactions between hydrophobic moieties on the carrier with hydrophobic  
 184 regions or domains on the protein. Thus, the pendant hydrophobic groups dominate the surface  
 185 chemistry of the carriers used for hydrophobic adsorption.
- 186 -Mostly chemical, dependent on the affinity of functional groups in the coating with the exposed  
 187 protein amino acid residues. Scheme 2 shows the main types of MNPs useful for protein  
 188 adsorption.

189 **Scheme 2.** Structure of MNPs used for protein immobilization.

190  
 191 An in-depth description of MNPs applied to protein separation are presented in next  
 192 section as a function of their surface chemistry.

### 193 **3.1. Iron oxide@metal-metal oxide**

194 Some proteins contain exposed amino acid residues capable of coordinating with  
 195 transition metals. Histidine (His) acts as an electron donor group and is present in the surface of  
 196 lactoferrin (Iyer et al., 1994), immunoglobulins (Al-Mashikhi et al., 1988), lactalbumin  
 197 (Berliner+ and Kaptein, 1980), lactoglobulin (Olsen et al., 2015) or BSA (Alaiz and Gir6n,  
 198 1994) in variable amounts. The affinity of His for copper ions has been utilized in column  
 199 chromatography for whey protein extraction with relative success. For example, lactoferrin and  
 200 immunoglobulin were separated from cheese whey by Cu-affinity chromatography (Al-  
 201 Mashikhi et al., 1988).  $\text{Cu}^{+2}$  ions were immobilized on 1,4-butanediol diglycidyl ether-  
 202 iminodiacetic acid and Sepharose 6B, packed into a column. Immunoglobulin adsorbed  
 203 strongly, unlike other proteins, and could be recover with 53 to 77 % purity. Better results were

204 obtained under the same chromatographic system for B-lactalbumin, which eluted after  
205 immunoglobulin. A purity of 90% and recovery of 80% was achieved, but it was necessary to  
206 reload the eluted protein on Cu-free matrix to clean it from leached metal (Blomkalns and  
207 Gomez, 1997). Cheese whey lactoferrin was directly captured with Cu<sup>2+</sup> on polyacrylamide  
208 cryogel-iminodiacetic acid. This was possible after ultrafiltration of the whey to get rid of the  
209 lighter proteins. Lactoperoxidase was a possible contaminant but it passed straight through the  
210 Cu<sup>2+</sup>-cryogel, while lactoferrin was retained and could be eluted with high purity (Carvalho et  
211 al., 2014). Artificially tagging proteins with this His or other amino acids is a common  
212 technique for adsorption enhancement (Wijekoon et al., 2016).

213 Regarding MNPs, transition metals have been attached onto diversely functionalized  
214 magnetic materials in order to potentiate the protein binding according to the previously  
215 mentioned antecedents. Cu<sup>+2</sup> ions were immobilized through EDTA on MAG and then  
216 contacted with a 2.0 mg.mL<sup>-1</sup> bovine hemoglobin (BHb) solution, a His-rich protein.  
217 Adsorption was maximum at pH 8 (1200 mg protein.g of carrier<sup>-1</sup> in one hour) and no  
218 significant effect was observed by variation of ionic strength. Specificity towards BHb was  
219 evaluated in a mixture together with lysozyme (Lyz) and BSA, which possess less surface-  
220 exposed His residues. 89.8% of BHb was removed from the mixture, whereas only 19 % of  
221 BSA and 15,9 % of Lyz attached to the particles (C. Ding et al., 2015). His-tagged Green  
222 Fluorescent Protein (GFP) could also be recovered by the same material up to 120 mg.g carrier<sup>-1</sup>  
223 per hour (Fraga García et al., 2015).

224 Nickel is another His-binding metal. NiO-decorated MNPs were successfully applied to  
225 His-tagged proteins with MAG-SiO<sub>2</sub> or MAG-Al<sub>2</sub>O<sub>3</sub> as starting materials (Li et al., 2015;  
226 Mirahmadi-Zare et al., 2016). Ni<sup>2+</sup> cation was immobilized on maghemite-glicidilpropyl-  
227 trimethylsilane-N,N-carboxymethyl-lysine. Upon repeated contact with a cell lysate from which  
228 to extract a His-tagged protein, the loss of particles was very high after the fourth cycle, leading  
229 to a low adsorption efficiency in the fifth cycle (Gädke et al., 2017).

230 A comparison between the lysozyme binding ability on carboxymethyl-chitosan-coated  
231 MAG modified with Fe<sup>+3</sup>, Zn<sup>+2</sup> or Cu<sup>+2</sup>, respectively, was reported. The higher efficiency was  
232 found employing Fe at pH 6 (232.56 mg/g vs 200 for Zn and 185 for Cu). Fe (III) ions have a  
233 strong affinity for oxygen containing functional groups such as carboxylic and phenolic oxygen,  
234 so the aspartic acid, glutamic acid and tyrosine residues which on the surface of the lysozyme  
235 molecules provides affinity-binding sites for Fe (III) ions through carboxylate and phenolic  
236 functional groups.

237 The elution strategy was, in principle, the increase of ionic strength using an aqueous  
238 solution of NaCl 0.2M. As it was not enough to achieve elution, imidazole was utilized as well  
239 It was found that using 0.2 M imidazole containing 0.2 M NaCl solution could recover more  
240 than 95% of the bound proteins (Sun et al., 2011a).

241 Unpublished own data confirms the results achieved by other authors regarding the  
242 synergic effect of Cu on MNPs structure. In our case, citric-acid-coated MNPs (CA-MAG)  
243 remove about 60 % of total whey proteins. Retreating the CA-MAG-processed whey with Cu<sup>2+</sup>-  
244 CA-MAG this percentage raised to 80 %. SDS-PAGE analysis showed that CA-MAG  
245 adsorption system exhibited a larger affinity for positively charged lactoferrin and  
246 lactoperoxidase. The reason for choosing Cu over Fe is merely cost-effective, since copper  
247 sulphate is about 30 % cheaper than iron(II) sulphate (prices in Argentina).

248 The articles dealing with transition-metal modified MNPs show the modifier as a  
249 suitable one to assess an efficient whey protein extraction. It is worth mention that few studies  
250 have been found in open literature evaluating diverse metals on different MNPs. From the  
251 analysis of those, hardly any conclusions can be drawn on this topic. It is necessary to plan more  
252 systematic research devoted to evaluate the adsorption capacity and selectivity of transition  
253 metals on the same magnetic matrix. Selection of the organic phase as coating of MNPs should

254 ponder a series of conditions such as high chemical and mechanical resistance in whey  
255 environment, stable metal uptake and low cost.

### 256 **3.2.Iron oxide@polymers**

257 The coating of MNPs with polymeric moieties is one of the most widespread strategy to  
258 increase the versatility of the magnetic systems providing specific properties to attain the  
259 desired applications. In the field of protein separation/immobilization and/or isolation a wide  
260 gamma of polymers, natural and synthetic, have been employed to magnetic phase  
261 functionalization. In general terms, aminated and/or carboxylated polymers are the preferred  
262 because of their affinity with protein moieties.

263 One of the most employed polymers is chitosan, a versatile biopolymer extensively used in  
264 the biomedical and the industrial fields for its biocompatibility and non-cytotoxicity (Choi  
265 et al., 2016). Magnetic chitosan composites have been widely studied for several  
266 applications, including proteins capture. In previous own works we have reported the  
267 efficient adsorption of BSA onto Fe<sub>3</sub>O<sub>4</sub>-chitosan particles (Nicolás et al., 2013). Similar  
268 findings were earlier achieved by employing magnetite chitosan and magnetite cellulose  
269 composites to assess the immobilization of BSA and insulin by simple adsorption  
270 mechanism. Proteins and chitosan (CS) particles presented opposite surface charge at the  
271 selected pH (5.7, distilled water). Electrostatic interactions are then expected to govern the  
272 BSA and insulin (negatively charged) adsorption on CS based supports (positive). On the  
273 other hand, cellulose particles are also negatively charged, hence not electrostatic but  
274 mainly physical and hydrophobic interactions (plus other Van der Waals forces such as H-  
275 bonding) are expected to maintain the proteins linked to those supports (Lassalle et al.,  
276 2011)

277 Other possibilities include the use of a crosslinking molecule to form covalent bonds,  
278 such as carbodiimide (Sadeghi et al., 2016). In this case, most of the offered BSA was  
279 incorporated but no elution tests were performed. This is a complex situation since the creation  
280 of covalent bonds between the protein and the carrier would require a harsh chemical treatment  
281 to reverse the reaction and recover the target biomolecule, impairing its integrity.

282 Carboxymethyl chitosan provided an appropriate compatibility with lysozyme. The  
283 biopolymer, anchored on MAG-poly-ethylene glycol particles, reached a 256.4 mg/g loading  
284 capacity. Due to the small diameter, the adsorption equilibrium was reached within barely  
285 20 min and fitted well with the Langmuir model (Sun et al., 2011b).

286 MAG coated with carboxymethyl cellulose was compared to chitosan-MAG in a  
287 peroxidase purification process. Both supports have a strong positive charge under the applied  
288 experimental conditions (pH=5), being even higher for chitosan-MAG. Nevertheless,  
289 carboxymethyl cellulose composite demonstrated to be the most efficient in terms of  
290 purification yield. The authors assigned this result to the larger surface area than the  
291 underivatized chitosan (Zengin Kurt et al., 2017).

292 Carboxyl -modified magnetic particles were prepared by polymerization of acrylamide  
293 with N, N'-methylenebisacrylamide in presence of magnetite particles under sonication. The  
294 resulting polymer exposed -COO<sup>-</sup> groups. Combinations of magnetic fishing and aqueous two-  
295 phase extraction (ATPE) were tested. The liquid extraction medium contained water, PEG4000  
296 and ammonium sulphate forming two phases after centrifugation. A mixture of BSA, lysozyme,  
297 cytochrome C and myoglobin (Mb) were treated in two different ways, exposing the proteins to  
298 magnetic fishing followed by extraction and vice versa (Gai et al., 2011). When magnetic  
299 particles were added to the proteins mixture, Cyt C and Lyz were adsorbed completely and BSA  
300 and Mb remained in solution. Then, adding the mixture of PEG and sulphate into the remaining  
301 solution, the top and bottom phase were formed. BSA and Mb were fully allocated in the  
302 bottom phase, and their concentrations were significantly higher than the original solution. It  
303 indicated that Cyt C and Lyz could be separated by magnetic particles adsorption directly, and  
304 the remained BSA and Mb were enriched by ATPE.



305 Superparamagnetic microspheres (3.2  $\mu\text{m}$ ) were obtained by coating magnetite with  
306 poly(glycidyl methacrylate) and further functionalized with ethylenediamine, exposing  $-\text{NH}_3^+$   
307 groups. Upon contact with a pure BSA solution at pH 7-7.5 over 150 mg of protein adsorbed per  
308 gram of carrier. More than 90 % of the attached BSA could be recovered by elution with 0.6 M  
309 NaCl (Liu et al., 2016).

310 In another extensive research, 12 different magnetic ion-exchangers were created by  
311 linking polyethyleneimine (PEI), trimethylamine or diethylamine ethyl chloride on MAG  
312 particles. The PEI support presented high loading capacity towards BSA (337 mg/g) in a model  
313 system, so it was selected for crude bovine whey treatment. The process consisted of using first  
314 a magnetic cation-exchanger (MAG-poly-glutaraldehyde-epichlorohydrin-sulphite) to adsorb  
315 basic protein, and the supernatant was then contacted with the PEI anion-exchanger. Desorption  
316 selectivity was subsequently studied by sequentially increasing the concentration of NaCl in the  
317 elution buffer. In the initial cation-exchange step quantitative removal of lactoferrin and  
318 lactoperoxidase was achieved with some simultaneous binding of immunoglobulins. The  
319 immunoglobulins were separated from the other two proteins by desorbing them with a low  
320 concentration of NaCl ( $\leq 0.4$  M), whereas lactoferrin and lactoperoxidase were co-eluted in  
321 significantly purer form, e.g. lactoperoxidase was purified 28-fold over the starting material,  
322 when the NaCl concentration was increased to 0.4–1M. The anion-exchanger adsorbed  $\beta$ -  
323 lactoglobulin selectively allowing separation from the remaining protein (Heebøll-Nielsen et al.,  
324 2004).

325 Numerous studies were carried out in the application of MNPs coated polymers to  
326 assess protein purification and immobilization. However, the specific separation and isolation of  
327 cheese whey proteins is more limited. Although cationic polymers seem to be more suitable,  
328 certainly any clear trend may be visualized because of the limited information in available  
329 literature.

### 330 **3.3.Iron oxide@bioaffinity ligand**

331 Diverse biomolecular moieties are currently employed as extraction sorbents. Such  
332 biomolecules may be linked to the magnetic surface by either covalent coupling and/or non-  
333 covalent interactions. These bioaffinity sorbents can be prepared using, for example, antibodies  
334 or aptamers, and may operate by a retention mechanism during the extraction based on  
335 molecular recognition. Other types of biological molecules present high affinity for a  
336 determined part of a molecule. For instance, Concanavalin A, a kind of protein with specificity  
337 to sugars, was immobilized on MNPs through carbodiimide. Since lactoferrin is a glycoprotein  
338 (contains oligosaccharide chains covalently attached to the polypeptide), the particles bonded  
339 selectively to it in presence of BSA: 58.12 mg lactoferrin/g vs. 0.8 of albumin. Elution was  
340 performed with a Tris buffer containing D-methylglucoside and NaCl (Lai et al., 2013).

341 For non-antibody proteins, often no natural partner is known with suitable properties for  
342 use as an affinity reagent (Béhar et al., 2016). The structure-based design of chemicals and  
343 peptidic mimetics is then an alternative to obtain artificial ligands for biological targets.  
344 Specifically, proteins artificially tailored for this purpose are called *affitins*. Few manuscripts  
345 have been published on this topic since it's a relatively new concept. Applications include  
346 purification of antibodies and non-immunoglobulin proteins (Béhar et al., 2016) and purification  
347 and detection of conformational changes of other proteins (Krehenbrink et al., 2008). Efforts are  
348 being oriented to the design of stable and functional affitins (Béhar et al., 2014; Miranda et al.,  
349 2011).

350 Anti-lysozyme and anti-IgG affitins were immobilized onto magnetic particles to assess  
351 their potential for protein purification by magnetic fishing. The optimal lysozyme and human  
352 IgG binding conditions yielded 58 mg lysozyme/g support and 165 mg IgG/g support,  
353 respectively. The recovery of proteins was possible in high yield ( $\geq 95\%$ ) and with high purity,  
354 namely  $\geq 95\%$  and 81%, when recovering lysozyme from *Escherichia coli* supernatant and IgG  
355 from human plasma, respectively (Fernandes et al., 2016).

356 The described entities may preferentially bind to protein A/G, lectins, enzymes, as well  
 357 as molecular receptors sensitive to molecular interactions with certain groups of molecules.  
 358 Hence, they can also be used as selective tools in extraction procedures (Pichon et al., 2012).

359

### 360 3.4. Miscellaneous magnetic nanomaterials

361 The classification regarding the nature of the magnetic phase modifier correlates to the  
 362 compounds most extensively used in open literature for these purposes. However other  
 363 modifiers/functionalizers less commonly reported are summarized in this section.

364 Table 2 lists different magnetic nanomaterials with uncommon or unspecific  
 365 modifications that have been tested for protein recovery.

366

367 **Table 2.** Uncommon magnetic nanomaterials applied to protein extraction

Material	Target proteins	Medium	Contact conditions	Results	Ref.
MAG-SiO <sub>2</sub> - HS <sub>2</sub> C <sub>3</sub> H <sub>6</sub> -Si- (EtO) <sub>3</sub>	BSA Lysozyme	Artificial solutions	10 mg particles + 1 mL protein (5 μM) in buffer (100 mM, pH 4.65, 7.5, and 11)	Both proteins adsorb. Amount of each pH- dependent	(Lee et al., 2012)
MAG-Au- organic acid	Lysozyme	Egg white	2 mg of Fe <sub>3</sub> O <sub>4</sub> /Au- acid NPs + 1 mL of diluted egg white, pH=10. 10 min at room T with shaking	346 μg protein /mg NPs. Total elution and reusability	(Zhu et al., 2016)
MAG-SiO <sub>2</sub> - 3Cl-triazine	BSA	Artificial solution	4 mg NPs +1 mL BSA 0.5 mg/mL room T 1-8 h	130 mg BSA/g NPs when 1 mg BSA is offered to 4 mg NPs	(Bordbar et al., 2014)

368

369 According to the contribution of Lee et al. (2012), low-molecular-weight proteins (i.e.,  
 370 LYZ) are earlier retained at the surface and are later displaced by relatively high-molecular-  
 371 weight ones. Besides this partial selectivity, in these particular systems, proteins were not  
 372 completely separated from particles even using 3 M NaCl. Treatment with 0.1 M glycine  
 373 solution (pH 2.3) was necessary to partially desorb them. Thus, -SH modified materials should  
 374 be ruled out as efficient whey proteins adsorbents.

375 MAG-gold NPs demonstrated suitable adsorption and desorption capacity for lysozyme  
 376 (Zhu et al., 2016). However Lyz concentration in whey is markedly lower than in egg white (<  
 377 1mg/L vs. 2.2 to 4.5 mg/mL (Vidal et al., 2005)), hence this behavior may not be  
 378 straightforwardly extrapolated to the CW residue. MAG-Au-organic acids particles are another  
 379 alternative deserving interest and not yet explored in real whey samples, for which its selectivity  
 380 towards other proteins is unknown. Nevertheless, the high fabrication costs associated to gold  
 381 nanomaterials is an important limitation when intending their application in large-scale whey  
 382 processing.

383 In the case of MAG-triazine particles (Bordbar et al., 2014), immobilization occurs  
 384 through a strong covalent bond. Recovery of pure protein would then imply a harsh chemical  
 385 treatment not suitable concerning the retention of whey proteins biological functions.

386 **4. Elution methodologies and recovery results**

387 In general terms, the elution of proteins from MNPs or other adsorbent material consists  
 388 of displacing the biomolecule by other chemical species with a stronger affinity for the solid  
 389 support. The requirements of this process are devoted to detach the protein, as well as to  
 390 maintain its integrity (structure, biological function) and purity for further eventual applications.

391 Different strategies are implemented to assess this goal. The most widely employed are  
 392 ionic strength increase, pH modification and ligand exchange with amino acids fractions, among  
 393 others less common. Sometimes, combinations of these methods are needed for a proper and  
 394 efficient elution. It is worth mention that the adopted strategy would completely depend on the  
 395 mechanism of adsorbent-protein retention.

396 Table 3 compares the efficiency of different elution methods for a particular protein  
 397 from several magnetic and not magnetic materials.

398 **Table 3.** Elution methods of whey proteins from solid supports

Protein	Elution method	Efficiency of elution % *	Adsorbent Support(s)	Reference
Lactoferrin	1 M NaCl in 20 mM sodium phosphate, pH 6	61,9	Both Lewatit MP500 anionic resin and Sepharose cationic resin into ethylene vinyl alcohol base polymer	(Saufi and Fee, 2011)
A-Lactoalbumin		14.9		
BSA		0		
Immunoglobulin G		72,6		
Lactoferrin	0.5 M NaCl in Phosphate buffer pH 6 20mM acetic buffer, pH 4.0	90 65	Superparamagnetic polyglycidyl methacrylate particles coupled with heparin	(Chen et al., 2007)
Lactoperoxidase	2 M NaCl in 20 mM acetate buffer pH 5.0	92	Sepharose 6B-reactive red 4 dye	(Urtasun et al., 2017)
Lactoperoxidase	Stepwise elution: 0.075 M NaCl, 0.15 M and 1 M in 10 mM phosphate buffer pH 5.8	92	Cation exchange composite cryogel embedded with cellulose beads	(Pan et al., 2015)
$\beta$ -Lactoglobulin	NaF 0.6 M in 10 mM phosphate buffer pH 6.25	100	Ceramic hydroxyapatite	(Schlatterer et al., 2004)
Lactoferrin	2 M NaCl in 25% ethylene glycol pH 7	99 80	Composite polymer membrane with Red HE-3B dye Agarose beads- Red HE-3B dye	(Wolman et al., 2007)

Lactoferrin	Temperature drop from 40 to 4 °C	76	Resin based on <i>N</i> -isopropylacrylamide	(Maharjan et al., 2016)
BSA	50 mM Tris/HCl, 1M NaCl, pH 8.0	88	MAG-polyethyleneimine anion exchanger	(Heebøll-Nielsen et al., 2004)
	50 mM sodium citrate, pH 3.5 (2 cycles each)	54		
Lactoferrin and Immunoglobulin G	0.05 M Tris-acetic acid containing 0.5 M NaCl, pH gradient 8.0 to 2.8	Not reported	Sepharose 6B-organic ligands-Cu <sup>2+</sup>	(Al-Mashikhi et al., 1988)

399 \*Percentage of eluted protein considering only the adsorbed amount, not the offered initial one.

400 Proteins are complex amphoteric molecules containing both negative and positive  
 401 charges, their net charge may be controlled by conveniently adjusting the pH of surrounding  
 402 media. This means that proteins can be separated on both anion and cation exchangers by  
 403 selecting the suitable pH of the used buffer. To achieve good separation the buffer pH should be  
 404 at least one pH unit above or below the isoelectric point of the protein (Abd El-Salam and El-  
 405 Shibiny, 2017). This procedure results efficient since the protein is linked to the adsorbent by  
 406 electrostatic interactions involving protonated/deprotonated groups. From Table 3 it is evident  
 407 that this is the main type of protein-MNP interaction.

#### 408 6. Comparison between different proteins adsorbents employed in different media

409 In this section, an integral comparison involving from retention to elution procedure is  
 410 presented considering available procedures for whey proteins isolation.

411 **Table 4.** Practical parameters of interest of different whey protein recovery methods

Separation method	Final product	Elution method	Recovery results	Ref.
UF membrane (polyethersulfone MW cut-off 10 kDa) + 4 cycles DF	Whey protein concentrate (mixture of all proteins)	Not applicable	72% protein product. No loss in permeate	(Baldasso et al., 2011)
Sepharose-iminodiacetate-Cu <sup>2+</sup>	Mostly A-LA some B-LG	Acetate buffer* in steps: pH 5.5, 5.0, 4.5, 3.8	80 % yield, 90% purity	(Blomkalns and Gomez, 1997)
Phenyl- modified hydrophobic resin	Mainly α-LA, some B-LG and casein	50 mM Tris 1.5 mM CaCl <sub>2</sub> pH 7.5	79 % purity	(Conrado et al., 2005)
(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub> precip. + Anion exchanger (Diethylaminoethyl cellulose)	α-LA, BSA and B-Ig	NaCl 0.1-0.4 M in 0.05 M Tris	Comparable to commercial standards (qualitatively)	(Neyestani et al., 2003)

		pH 6.5 (removes Ig)	estimated by PAGE)	
	Gel filtration (Sephadex G-50)	20 mM PO <sub>4</sub> <sup>3-</sup> buffer, pH 8.6 (separates BSA from LA)		
	MAG-GLUT- epichlorohydrin- SO <sub>3</sub> <sup>-</sup>	Mostly LPO and some LF	1 M NaCl in 10 mM PO <sub>4</sub> <sup>3-</sup> buffer pH 7	>90% LPO capture, purified 36-fold and concentrated 4.7-fold. (Heebøll-Nielsen et al., 2004)
	Sepharose 6B- Red 4 dye	LPO, minimum LF	2 M NaCl in 20 mM acetate buffer  pH 5.0	86.5 % yield, >80 % purity (Urtasun et al., 2017)
	Cation exchange composite cryogel embedded with cellulose beads	LPO	Stepwise:  NaCl 0.075 M, 0.15 M and 1 M in 10 mM phosphate buffer  pH 5.8	>98% purity (Pan et al., 2015)
	MAG- carbodiimide- Concanavalin A	LF	0.02M Tris buffer with 0.2 M α-D- methylgluc oside and 0.5 M NaCl pH 7.4	Highly selective in presence of BSA (Lai et al., 2013)
	MAG-Anti- lysozyme affitin	Lysozyme (from cell lysate)	100 mM glycine- HCl buffer, 0.15 M NaCl, pH 2.5	≥95% yield ≥95% purity (Fernandes et al., 2016)

412 UF=ultrafiltration DF=diafiltration

413 \*not clear if buffer contains NaCl

414 Surprisingly, no information about reuse of the adsorbents is reported in the cited publications,  
415 although all of them have that potential.

## 416 7. Conclusions and prospects

417 Extracting whey proteins by means of magnetic fishing represents an attractive  
418 alternative among the traditional ones because of several advantages such as:

419 -Simplification of reactor design

420 -Facile and time-saving magnetic decantation (indistinctly of the volume of whey) vs. long  
421 loading times related to large volume of whey passing through narrow columns or membranes.

422 -Low-cost starting materials and simple preparation methods of MNPs

423 -Chemical and mechanic resistance enabling potential long-term reusability

424 A great volume and more exhaustive, experimental and theoretical, studies are currently  
425 required in order to assess the real potential of this novel technology to provide added value to a  
426 large residue such as the cheese whey. The purpose of this review is to raise awareness on the  
427 topic establishing the starting point for the exploration of favorable experimental conditions and  
428 improvements related to use and optimization of performance in protein separation. The real  
429 interest is in revalorizing the isolated proteins from wastes by low cost, simple and green-made  
430 nanotechnological materials.

431 The take-home message of this review is that, currently, the most effective techniques  
432 for whey protein recovery include the combination of molecular-size-based membrane filtration  
433 and affinity chromatography. Membranes involve thorough maintenance to avoid fouling.  
434 Specific columns are not suitable for industrial-scale volumes of whey, not to mention their  
435 elevated price.

436 MNPs arise as a cheap, versatile and reusable material for the rational design of whey  
437 protein adsorption systems. Besides, their production and final disposition are environmentally  
438 friendly.

439 There are still vacancy areas: there is no single procedure able to treat whey and isolate  
440 proteins. The main necessity is to develop *low-cost* magnetic adsorption systems for whey  
441 proteins recovery optimizing elution conditions to maximize selectivity and yield.

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**Highlights**

- Cheese whey proteins isolation is a complex and expensive process
- No single procedure is capable of complete whey treatment
- Magnetic nanoparticles are cost-effective and reusable adsorption systems
- Magnetic decantation enables facile protein separation from whey
- Magnetic adsorption systems are a feasible alternative to filtration or chromatography



$N_2$

NaOH

$Fe^{3+}$ ,  $Fe^{2+}$ ,

citric acid,  $70\text{ }^\circ\text{C}$

