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# Catalyst-free Ethyl Biodiesel Production from Rice Bran under Subcritical Condition

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**Abstract.** In-situ ethyl biodiesel production from rice bran under subcritical water and ethanol with no catalyst was employed. This process is environmentally friendly and is very flexible in term of feedstock utilization since it can handle relatively high moisture and free fatty acids (FFAs) contents. In addition, the alcohol, i.e. bioethanol, is a non-toxic, biodegradable, and green raw material when produced from non-edible biomass residues, leading to a 100% renewable biodiesel. The fatty acid ethyl esters (FAEEs, ethyl biodiesel) are better than fatty acid methyl esters (FAMES, methyl biodiesel) in terms of fuel properties, including cetane number, oxidation stability and cold flow properties. The influences of the operating variables such as reaction time (1 – 10 h), ethanol concentration (12.5 – 87.5%), and pressurizing gas (N<sub>2</sub> and CO<sub>2</sub>) on the ethyl biodiesel yield and purity have been investigated systematically while the temperature and pressure were kept constant at 200 °C and 40 bar. The optimum results were obtained at 5 h reaction time and 75% ethanol concentration using CO<sub>2</sub> as compressing gas. Ethyl biodiesel yield and purity of 58.78% and 61.35%, respectively, were obtained using rice bran with initial FFAs content of 37.64%. FFAs level was reduced to 14.22% with crude ethyl biodiesel recovery of 95.98%. Increasing the reaction time up to 10 h only increased the yield and purity by only about 3%. Under N<sub>2</sub> atmosphere and at the same operating conditions (5h and 75% ethanol), ethyl biodiesel yield and purity decreased to 54.63% and 58.07%, respectively, while FFAs level was increased to 17.93% and crude ethyl biodiesel recovery decreased to 87.32%.

**Keywords:** Ethyl biodiesel; rice bran; in situ; subcritical water; subcritical ethanol.

## INTRODUCTION

As a country with rice as staple food, Indonesia has abundant quantity of rice bran which is a by-product of rice milling. Rice bran is naturally rich in oil, polysaccharide, protein, fiber, vitamin and antioxidant; however it is traditionally only utilized as low value cattle food. The oil content in rice bran is affected by the degree of milling, but it is typically around 10 – 25% [1 – 3]. This high oil content and the fact that the oil is rather unsuitable for human consumption due to high free fatty acids (FFAs) content [4] make rice bran suitable for biodiesel feedstock.

Traditionally, biodiesel is produced by reacting oil and alcohol with strong base as a catalyst. However, this process requires less than 1% FFAs content in feedstock [5], otherwise soap will be formed making the separation process complicated. Therefore, this process is unsuitable for crude rice bran oil (RBO) with high FFAs content. Oil with high FFAs content can be converted into biodiesel under acidic condition, but the reaction rate is quite low [2]. The transesterification reaction can also be catalyzed by enzyme; however the high cost of enzyme makes this route uneconomical [6].

Saka and Kusdiana [7] proposed non-catalytic transesterification of oil under supercritical alcohol condition to produce biodiesel. Their result showed that this method was not affected by FFAs and water contents. High conversion rate (> 95%) can be achieved within a few minutes. Nevertheless, this method requires high temperature (300 – 350 °C) and high pressure (200 – 350 bar) which may cause high operating cost in large scale.

Recently, several researchers have reported promising non-catalytic biodiesel production under subcritical alcohol-water condition using various feedstocks, e.g. soybean oil [8], algae [9] and activated sludge [10]. Subcritical water is defined as hot water under critical temperature (100 – 374 °C) and pressure high enough to maintain water at liquid state. Subcritical water has lower dielectric constant than that at ambient temperature, i.e. 27 at 250 °C and 80 at room temperature [8], and therefore can be used as an alternative solvent to extract organic compounds. Besides that, the dissociation constant of water ( $k_w$ ) at subcritical condition is higher than that at ambient condition, i.e.  $10^{-12}$  at subcritical condition and  $10^{-14}$  at ambient condition [11]. This will enhance the hydrolysis and transesterification reactions due to higher  $H^+$  and  $OH^-$  concentrations.

Subcritical water can be utilized to extract oil and other components in rice bran, such as polysaccharide, protein, vitamin and antioxidant. Using a biorefinery approach to maximize the value added of rice bran, the protein, vitamin and antioxidant can be isolated, while the polysaccharide can be employed as fermentation feedstock to produce ethanol. Biodiesel can also be produced simultaneously during extraction process by introducing alcohol into subcritical water. Although methanol is usually used in biodiesel production due to faster reaction rate and higher yield, ethanol can also be used as an alternative. The addition of ethanol into subcritical water can increase the recovery rate of non-polar compounds, such as oil, vitamin and antioxidant since the polarity of ethanol is closer to those of organic compounds than that of water.

Due to time limitation, only the production of biodiesel is reported in this work, while the isolation of other valuable compounds will be investigated in the future. The objective of this work is to investigate the effects of reaction time, ethanol concentration, and compressing gas type ( $CO_2$  and  $N_2$ ) on the in-situ production of ethyl biodiesel (fatty acid ethyl esters, FAEs) from rice bran using subcritical ethanol/water mixture. The experiments were carried out at constant temperature and pressure, i.e. 200 °C and 4 MPa.

## EXPERIMENTAL

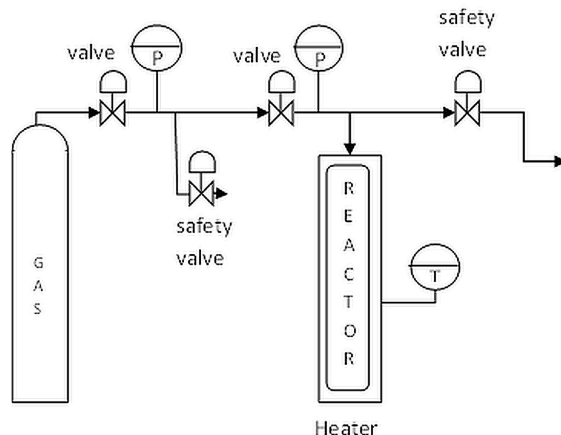
### Materials

Rice bran with  $12.9 \pm 0.1\%$  moisture and  $14.9 \pm 0.2\%$  oil contents was obtained from local rice mill (Lamongan, East Java, Indonesia). It is from IR 64 rice variety. The moisture content was determined by drying the rice bran while the oil content was determined by Soxhlet extraction using n-hexane as solvent for 5 hours. The free fatty acids (FFAs) in the rice bran oil were determined by using titration method according to a modified AOCS method [12] and it was found to be  $37.6 \pm 0.2\%$ .

All chemicals were analytical grades and purchased from Brataco (Indonesia). The compressing gasses ( $CO_2$  and  $N_2$ ) were supplied by Genta Prima Gas (Indonesia). Distilled water was used in this work.

### In-situ production of ethyl biodiesel

The oil extraction from rice bran and subsequent reaction with ethanol were carried out using subcritical ethanol/water mixture in a hydrothermal reactor. The reactor is made of seamless tubing 3/4" OD x 0.083 WT (SS-T12-S-083-6ME, Swagelok). The experimental setup is shown in Fig. 1.



**Figure 1.** Schematic diagram of experimental setup

Rice bran (5 g) was mixed with ethanol/water mixture (40 ml) in the reactor. The ethanol concentration was varied from 12.5 – 87.5%. The temperature was then raised to 200 °C by using an electric heater while the pressure was increased to 40 bar using either CO<sub>2</sub> or N<sub>2</sub> as compressing gas. After reaching the desired values, the temperature and pressure were maintained for a predetermined reaction time (1 – 8 h). The reaction was stop by quenching the reactor into an iced water bath to decrease both temperature and pressure to 5 – 15 °C and less than 5 bar, respectively. The needle valve was then released to reduce the pressure to atmospheric.

After that, the solid and liquid phases were separated. The liquid phase was mixed with hexane and stirred at 100 – 300 rpm for 10 minutes. After settled for 10 minutes, the hexane phase (top phase) was collected. The bottom phase was remixed with hexane and this procedure was repeated five times. The solid phase was also mixed with hexane, stirred at 100 – 300 rpm for 10 minutes and then the solid phase was separated from the hexane phase using filter paper. This procedure was also repeated five times. Subsequently, the hexane was evaporated in a rotary evaporator to recover the oil. The rice bran oil (RBO) obtained using this method was compared to that obtained using Soxhlet extraction with hexane to determine the recovery rate.

### Analysis of FFAs

The FFAs content was analyzed using titration method according to modified AOCS official method Ca 5a-40 as reported by Rukunudin et al. [12]. Crude ethyl biodiesel (0.01 g) was mixed with 96% ethanol (0.107 ml) and pp indicator (2 drops) in an Erlenmeyer flask. The mixture was heated to 50 °C and then titrated using 0.0044 N NaOH solution until the mixture turned to pink. The FFAs content was determined according to the following equation:

$$\%FFAs = [(Volume\ NaOH \times Normality\ of\ NaOH \times 28.2)/sample\ weight] \times 100\% \quad (1)$$

### Analysis of ethyl biodiesel content

The ethyl biodiesel (FAEEs) content in oil phase was determined using gas chromatography (GC) (HP 6890, Hewlett-Packard Inc., Avondale, PA, USA) equipped with a FID detector. Separation was carried out on a HP 1 crosslinked methyl siloxane column (60 m x 0.25 mm i.d. x 1 μm film thickness, Hewlett-Packard Inc., Avondale, PA, USA). The sample (0.02 g) was diluted in n-hexane (1 ml) and then was injected (0.5 μL) to the GC column. The injector and detector temperatures were set initially at 125 °C and were increased at a rate of 15 °C/minutes. After reaching 275 °C, the temperatures were held constant for 10 minutes. The flow rate of carrier gas (helium) was set at 28 ml/minutes at 200 °C. The yield of FAEEs was determined as the weight ratio of FAEEs to that of oil in rice bran as follows:

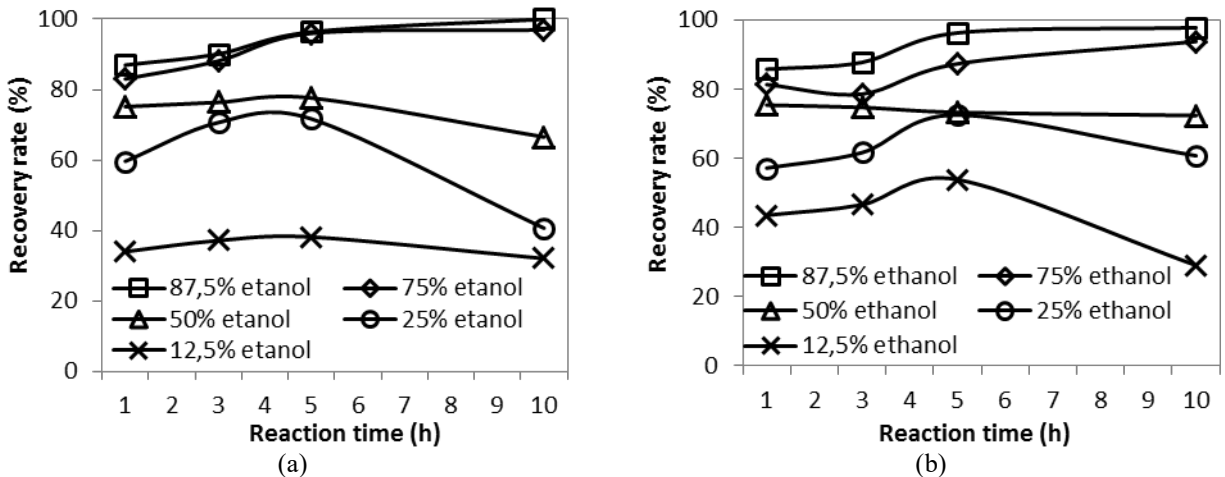
$$FAEEs\ yield\ (\%) = [ \{ sample\ weight\ (g) \times FAEEs\ content\ (\%) \} / oil\ weight\ in\ rice\ bran\ (g) ] \times 100\% \quad (2)$$

## RESULTS AND DISCUSSION

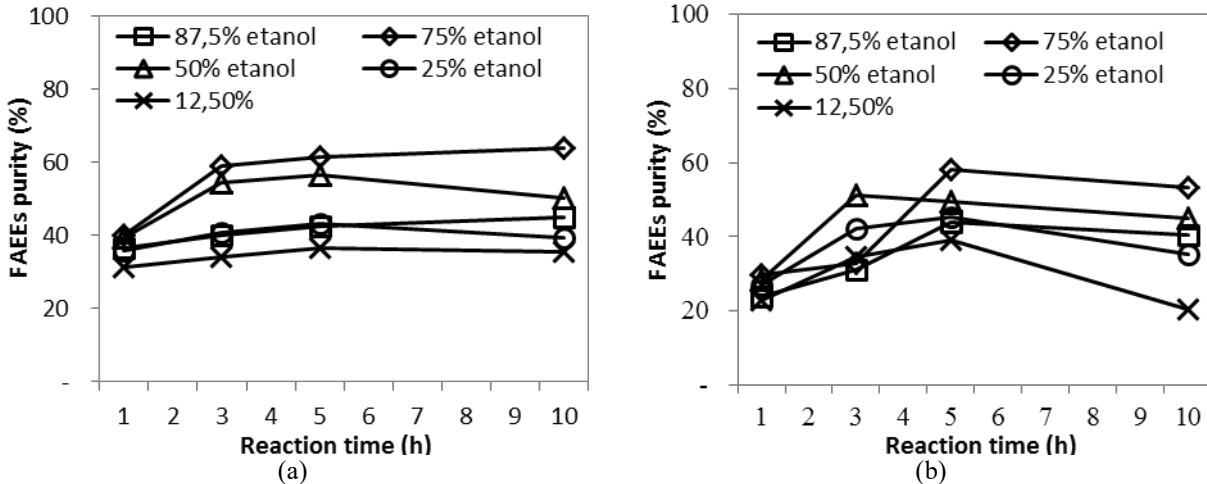
The effects of reaction time and ethanol concentration on the recovery rate of crude ethyl biodiesel under CO<sub>2</sub> and N<sub>2</sub> atmospheres are shown in Fig. 2(a) and (b), respectively. The experimental results show that the recovery rate is not significantly affected by the type of compressing gas used. In both cases, the recovery rate increases with increasing ethanol concentration and longer reaction time up to 5 h. Higher ethanol concentration is expected to increase the recovery rate since the polarity of ethanol is closer to that of rice bran oil than that of water and consequently, the extraction rate increases with higher ethanol concentration. At ethanol concentration lower than 75%, the recovery rate decreases when the reaction time is extended to 10 h, while at 75% and 87.5% ethanol concentrations, the recovery rates increase slightly. Under CO<sub>2</sub> atmosphere, the recovery rates at 87.5% ethanol concentration after 5 and 10 h reaction times are 96% and 100%, respectively. Therefore, the optimum reaction time can be considered to be 5 h.

The effects of reaction time and ethanol concentration on the ethyl biodiesel (FAEEs) purity in the crude biodiesel under CO<sub>2</sub> atmosphere is shown in Fig. 3(a). FAEEs purities at different ethanol concentrations increase with reaction time up to 5 h and then they are practically constant with longer reaction time. These results confirm that the optimum reaction time is 5 h. FAEEs purity also increases with increasing ethanol concentration up to 75%. Higher ethanol concentration increases the rates of both transesterification and esterification reactions as well as pushes the equilibrium toward the formation of FAEEs. However, increasing the ethanol concentration to 87.5% decreases FAEEs purity significantly. This may suggest that water has an important role in the formation of FAEEs under subcritical ethanol/water mixture. Saka and Minami [13] reported that the hydrolysis reaction is about four times faster than transesterification reaction, while the esterification of fatty acids was about an order of magnitude faster than transesterification reaction. Therefore, water is required to hydrolyze triglycerides into FFAs which subsequently react with ethanol to form FAEEs. This could be the preferred reaction mechanism under subcritical ethanol/water condition. These results also indicate that the presence of both water and FFAs is not a problem in subcritical ethanol/water method. Based on the experimental results, the optimum ethanol concentration is found to be 75%.

The behaviors under N<sub>2</sub> atmosphere show similar trend (Fig. 3(b)), however the FAEEs content is higher under CO<sub>2</sub> atmosphere at the same ethanol concentration. CO<sub>2</sub> can react with water to form carbonic acid making the solvent (ethanol/water mixture) acidic. Since hydrolysis, esterification and transesterification reactions are catalyzed by H<sup>+</sup>, the reaction rates are faster under CO<sub>2</sub> atmosphere.

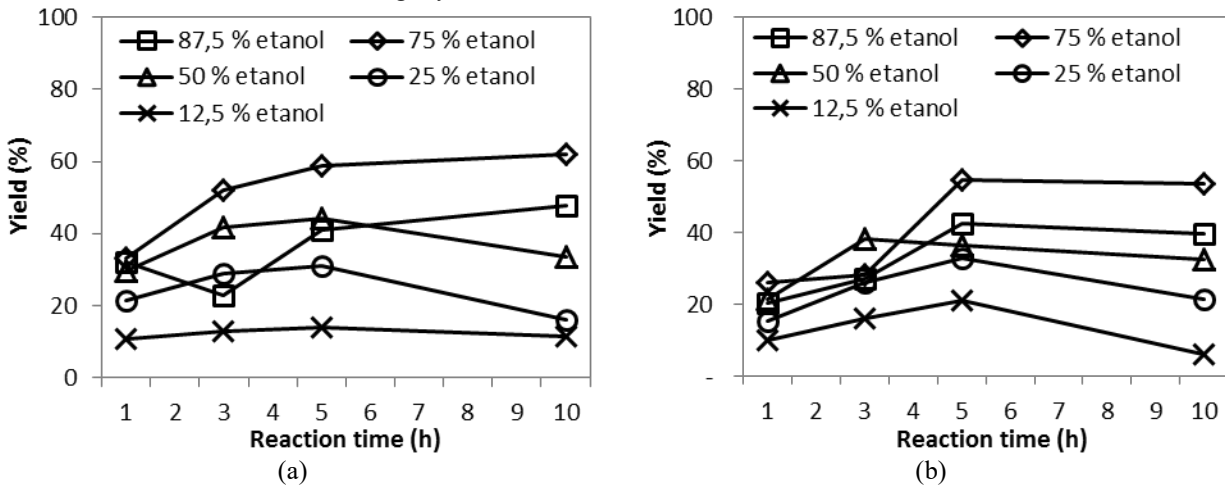


**Figure 2.** Effects of reaction time and ethanol concentration on the recovery rate of crude ethyl biodiesel (a) under CO<sub>2</sub> atmosphere and (b) under N<sub>2</sub> atmosphere. Operating conditions: T = 200 °C, P = 40 bar.



**Figure 3.** Effects of reaction time and ethanol concentration on the purity of ethyl biodiesel (FAEEs) (a) under CO<sub>2</sub> atmosphere and (b) under N<sub>2</sub> atmosphere. Operating conditions: T = 200 °C, P = 40 bar.

Figures 4(a) and (b) shows the FAEEs yields under CO<sub>2</sub> and N<sub>2</sub> atmospheres, respectively. FAEEs yield is defined as the ratio of FAEEs weight in the crude biodiesel to total oil weight in rice bran (obtained using Soxhlet extractor with hexane). FAEEs yield under CO<sub>2</sub> atmosphere is higher than that under N<sub>2</sub> atmosphere in accordance with higher FAEEs content under CO<sub>2</sub> atmosphere. While the maximum FAEEs yield of 62% is obtained after 10 h reaction time at 75% ethanol concentration (under CO<sub>2</sub> atmosphere), FAEEs yield at the optimum reaction time of 5 h and 75% ethanol concentration is slightly lower, i.e. 59%.

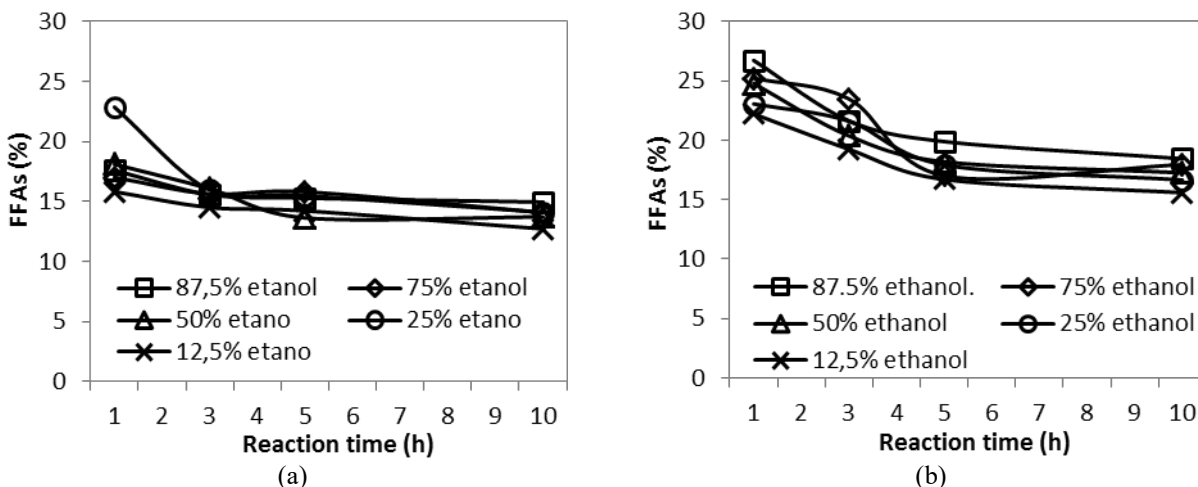


**Figure 4.** Effects of reaction time and ethanol concentration on the yield of ethyl biodiesel (FAEEs) (a) under CO<sub>2</sub> atmosphere and (b) under N<sub>2</sub> atmosphere. Operating conditions: T = 200 °C, P = 40 bar.

One of the main impurities in crude biodiesel is FFAs. FFAs contents under CO<sub>2</sub> and N<sub>2</sub> atmospheres are shown in Fig. 5(a) and (b), respectively. The experimental data show that FFAs content decreases with longer reaction time but ethanol concentration has little effect. FFAs contents under CO<sub>2</sub> atmosphere at 1 and 10 h reaction times are 15 – 23% and 12 – 15%, respectively, at different ethanol concentrations. Under N<sub>2</sub> atmosphere, the decrease in FFAs contents is more pronounced in the first 5 h of reaction, but the final FFAs contents are slightly higher than those under CO<sub>2</sub> atmosphere, i.e. about 15 – 18.5%. This is expected since esterification of FFAs is catalyzed by acid and CO<sub>2</sub> atmosphere can make the solvent more acidic.

The experimental data show that even after 1 h of reaction, the FFAs contents under both CO<sub>2</sub> and N<sub>2</sub> atmospheres are already significantly lower than that initially in the crude rice bran oil, i.e. 37.6%. This shows that this method can handle feedstock with high FFAs content efficiently so that pretreatment is not required. However,

even after 10 h reaction time, not all FFAs can be converted into FAEs. This is due to the presence of water in the system that hydrolyzes FAEs into FFAs and ethanol. It is the reverse reaction of FFAs esterification.



**Figure 5.** Effects of reaction time and ethanol concentration on FFAs content (a) under CO<sub>2</sub> atmosphere and (b) under N<sub>2</sub> atmosphere. Operating conditions: T = 200 °C, P = 40 bar.

## CONCLUSIONS

The effects of reaction time, ethanol concentration and compressing gas type on direct production of ethyl biodiesel (FAEEs) from rice bran using subcritical ethanol/water mixture have been investigated. It was found that crude ethyl biodiesel recovery rate, FAEEs content, FAEEs yield increased with reaction time, while FFAs content decreased. The optimum reaction time was found to be 5 h since longer reaction time up to 10 h only slightly increased the yield. The use of CO<sub>2</sub> as compressing gas led to higher FAEEs content and yield but lower FFAs content than those under N<sub>2</sub> atmosphere. This is because CO<sub>2</sub> can react with water to form carbonic acid making the solvent more acidic making the reactions faster since they are catalyzed by H<sup>+</sup>. However, the crude ethyl biodiesel was not significantly affected by the type of compressing gas used.

The crude ethyl biodiesel recovery rate increased with increasing ethanol concentration since the polarity of ethanol is closer to that of rice bran oil than that of water and therefore higher ethanol concentration increased oil extraction rate. FAEEs content and yield also increased with ethanol concentration up to 75%. Higher ethanol concentration increased both transesterification of oil and esterification of FFAs as well as pushes the equilibrium toward the formation of FAEEs. On the other hand, the FFAs content was not significantly affected by ethanol concentration.

The experimental results showed that subcritical ethanol/water mixture can be used to produce ethyl biodiesel from feedstock with high moisture and FFAs contents without any pretreatment. Besides that, this method is also catalyst-free. Therefore, this experiment can provide an efficient and environmentally friendly method to produce biodiesel from an abundant rice milling by-product, i.e. rice bran which has low economic value.

## ACKNOWLEDGMENTS

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