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1	Physical modelling of forest fire spreading through
2	heterogeneous fuel beds
3	
4	Suggested running head: Fire spread through heterogeneous fuels
5	
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13	
14	Abstract
15	Vegetation cover is a heterogeneous medium composed of different kinds of fuels and non-
16	combustible areas. Some properties of real-fires arise from this heterogeneity. Creating
17	heterogeneous fuel areas may be useful both in land management and in fire fighting by
18	reducing the fire intensity and the fire rate of spread. The spreading of a fire through a
19	heterogeneous medium was studied by a two-dimensional reaction-diffusion physical model
20	of fire spread. Randomly distributed combustible and non-combustible square elements
21	constituted the heterogeneous fuel. Two main characteristics of the fire were directly
22	computed by the model: the size of the zone influenced by the heat transferred from the fire
23	front and the ignition condition of vegetation. The model was able to obtain rate of fire
24	spread, temperature distribution and energy transfers. The influence on the fire properties of

25 the ratio between the amount of combustible elements to the total amount of elements has 26 been studied. The results provided the same critical fire behaviour as described in both 27 percolation theory and laboratory experiments but the results were quantitatively different 28 because the neighbourhood computed by the model varied in time and space with the 29 geometry of the fire front. The simulations also qualitatively reproduced fire behaviour for 30 heterogeneous fuel layers as observed in field experiments. This study shows that physical 31 models can be used to study fire spreading through heterogeneous fuels and some potential 32 applications are proposed about the use of heterogeneity as a complementary tool for fuel 33 management and fire-fighting.

34

35 Additional keywords: Fire critical behaviour, non-combustible zones, reaction-diffusion
36 model, surface fire spread.

37

38 Introduction

39 The main physical forest fire spread models describe the fire spreading through homogeneous 40 fuels (Pastor et al. 2003). However in the field, homogeneous fuel beds are extremely rare 41 (Brown 1982); vegetation cover is a heterogeneous medium including different kinds of fuels 42 and non-combustible areas (Bradstockl and Gill 1993). Some of the fires' properties can arise 43 from this heterogeneity, for instance, the development of fire fingers (Caldarelli et al. 2001). 44 Real-fires also display thresholds for spreading that depend on environmental factors such as 45 wind and fuel moisture content (Cheney et al. 1993, Marsden-Smedley et al. 2001, Weise et 46 al. 2005). The fire regimes are partly a consequence of a coupling between heterogeneous 47 patterns of vegetation and past fires (Baker 1989, Miller and Urban 1999). 48 The work described in this paper is motivated by the necessity of developing new

49 approaches in land management and in fire-fighting. The field experience of the first two

authors as fire-fighters has shown them that fire-fighting as well as fuelbreaks can become
ineffective during extreme events (strong winds, large-scale fires or steep canyons for
instance). Artificially controlling the fuel heterogeneity may be useful to reduce fire hazard
(Loehle 2004, Finney et al. 2007).

The critical behaviour of forest fires has been investigated in details thanks to the percolation theory (Stauffer, 1985). This approach allows better understanding of the forest fire behaviour at the field scale (Ohtsuki and Keyes 1986, Von Niessen and Blumen, 1986) and the interactions between fires and forest growth (Drosswel and Schwabl, 1992, Malamud et al. 1998). Other studies focused on the critical behaviour of fire spreading at the laboratory scale (Beer and Enting 1990, Nahmias et al. 2000).

In percolation-type models, the assumptions used to propagate the fire are not 60 61 physically based (Weber 1990) and the critical thresholds are directly dependent on the 62 assumptions made to build the models; this has been recognised as quite naive (Beer and 63 Enting 1990). For instance, the probability of ignition of a tree or the definition of the 64 neighbourhood of a burning plot – that is to say the other pieces of vegetation influenced by 65 this burning plot – are constant in space and time. These quantities must be known *a priori*. In 66 a real fire they vary with time and position. They also depend strongly on the fire front geometry and on vegetation as a fuel. This approach has permitted the modelling of the 67 68 critical behaviour of forest fires at the landscape scale, and they are used to study the long-69 term interaction with forest growth and fire (Drossel and Schwabl 1992). The application of 70 percolation-type fire spread models to the study of single fires is more limited because they 71 do not provide the primary outputs, such as rate of fire spread or heat fluxes, which are 72 necessary for forest managers and fire-fighters. Furthermore these models are very difficult to 73 validate as, in real fires it is difficult to discriminate percolation effects from the influence of

the external conditions (wind, vegetation moisture content, topography and so on, see
Tephany and Nahmias 2002 and Weise et al. 2005).

A recent approach based on the Small World Network combines physical modelling and percolation theory (Zekri et al. 2005). It provides very short calculation times but it necessitates the implementation of some physical parameters, as combustion time, time of degradation before ignition and long-range radiation effects. These parameters are obtained from physical modelling but they do not vary with time, position and front shape.

More recently, empirical fire spread models were used to assess the influence of heterogeneities made by prescribed burnings on the occurrence of unexpected fires (King et al. 2008). The results showed the role of heterogeneous fuels in decreasing fire size and intensity; they highlighted the need for more studies of this kind.

A convenient way to simulate the fire spread through heterogeneous fuel layers is by using Cellular Automata. They use a cellular mesh with each cell having a defined state (such as burned and unburned), a neighborhood and rules for the change in cell state. The rules use mathematical formulas to define the change in sate of the cells along time. The rules are based on the fire spread mechanisms. To define the rules, some approaches use percolation (Duarte et al. 1992) and others use semi-empirical models (Berjak and Hearne 2002). A detailed analysis can be found in the reviews by Perry (1996) and Sullivan (2009).

The main objective of this paper is to evaluate the ability of physical modelling to study the properties of wildland fire spreading through heterogeneous fuels. To proceed, a two-dimensional reaction-diffusion model was used. The model includes a sub-model for long-range radiative transfer and was validated at the laboratory scale for homogeneous fuel beds (Morandini et al. 2005). The study focused on the properties of a single fire spread. The non-homogeneous fuel consisted of combustible and non-combustible square elements randomly distributed with a fixed ratio. Such a model (and physical models generally) directly

determines the neighbourhood thermally influenced by the fire front and the ignition of
vegetation from physical considerations. These quantities are dependent on many parameters,
such as vegetation species, moisture contents, wind, slope and so on. The model also provides
the fire rate of spread, the temperature distribution, as well as the energy transfers. In this
paper, the model simulations were qualitatively compared to experimental results and studies
conducted both at laboratory and field scales.

In the next sections, the reaction-diffusion model and the numerical implementation are detailed. Results of simulations representing different kind of fuel heterogeneities are then presented and discussed; the simulations are compared qualitatively with theory and experiments. A short discussion is then conducted about the potential applications for fuel management and fire fighting that arise from this study. Finally, the conclusions are drawn and some scientific perspectives are proposed.

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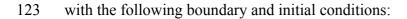
112 Numerical modelling

113 *The physical model*

The main characteristics of the model are summarized below. Further details are available inthe paper by Morandini et al. (2005).

The model has been developed to represent the fire spread through fuel beds (such as pine needle beds) and it has been validated at laboratory scale in terms of rate of spread, temperature, fire front shape and heat transfer. It takes into account the thermal transfers that are involved in the field, including long-range radiation. Thus, this model can be considered suitable for bench-scale modelling of the fire spread through heterogeneous fuels in the field. The main equation is a thermal balance on a medium equivalent to the fuel bed:

122
$$\frac{\partial T}{\partial t} + k_v \vec{V}_g \cdot \vec{\nabla} T = -k(T - T_a) + K \Delta T - Q \frac{\partial \sigma_k}{\partial t} + R$$
(1)



124	$\vec{n}.\vec{\nabla}T = 0$	at the fuel-bed boundaries,	(2)
125	$T_0 = T_a$	for an unignited cell at time zero,	(3)
126	$T_0 = T_{ig}$	for an ignited cell at time zero.	(4)

127 Load variation along time for a burning cell is represented by:

128
$$\sigma_k = \sigma_{k_0} e^{-\alpha(t-t_{ig})}$$
(5)

129 where T and T_a represent the equivalent medium temperature and the ambient temperature 130 respectively. The ignition time t_{ig} is defined as the time when the cell temperature reaches the 131 ignition temperature. k is the cooling convection coefficient, K is the equivalent diffusion 132 coefficient, Q is the combustion enthalpy and α is the combustion time constant. The 133 coefficients of Eq. 1 are reduced coefficients as they are divided by the thermal mass per unit 134 area of the medium equivalent, m. The model parameters $(k, K, Q \text{ and } \alpha)$ are determined from 135 a measured time-temperature curve obtained for a linear spread under no slope and no wind 136 conditions (Santoni et al. 1999). The advective coefficient k_v is estimated as a thermal mass 137 ratio (Simeoni et al. 2003). σ_k and σ_{k_0} are the fuel load and the initial fuel load, respectively. 138 The radiative and convective terms are described in greater detail below.

With regard to the radiation term *R* in Eq. (1), the flame is assumed as being a radiant surface with a given height and constant temperature T_{fl} and emissivity ε_{fl} (Morandini et al. 2001). The amount of energy impinging the top of the fuel layer was calculated from the Stefan-Boltzmann law. The rate at which radiant energy from flame front is absorbed by the fuel element dS_v is:

144
$$\phi_{\beta - dS_{\nu}} = a_{\nu} \varepsilon_{\beta} B T_{\beta}^{4} F$$
(6)

145 where *B* is the Stefan-Boltzmann constant and a_v is the fuel bed coefficient of absorption. The 146 view factor *F* depends on the flame length and tilt angle as follows (cf. Fig. 1):

147
$$F = \int_{S_{fl}} \frac{\cos\varphi_{fl} \cos\varphi_{k}}{\pi r^{2}} dS_{fl} dS_{k}$$
(7)

148 Thus we obtain:

149 R = 0 for a burning cell, (8)

150
$$R = \frac{\varphi_{fI-dS_v}}{m dS_v} = R^* F \qquad \text{for an unburned cell located ahead of the fire front,} \tag{9}$$

151 where *m* represents the thermal mass of the fuel per unit area.

152 To express the convective term present in Eq. (1), the following equations for the flow153 through the fuel layer are set (Simeoni et al. 2003):

154
$$\frac{\partial V_{g,x}}{\partial x} + \frac{V_{g,x}}{\rho_g} \frac{\partial \rho_g}{\partial x} = -\frac{V_{g,z}(\delta)}{\delta} - \frac{1}{\rho_g \delta} \frac{\partial \sigma_k}{\partial t} \qquad \text{in the burning zone,} \tag{10}$$

155
$$V_{g,z}(\delta) = \chi \sqrt{2\delta \left(\frac{T}{T_a} - 1\right)g \cos \phi_{sl}} \qquad \text{in the burning zone,} \qquad (11)$$

156
$$\rho_g T = \rho_a T_a$$
 in the gas phase, (12)

were δ is the height of the fuel layer, ϕ_{sl} is the slope angle and χ is a drag forces coefficient 157 158 (Simeoni et al. 2003). The model presented in Eqs. (1-9) is two-dimensional along the ground 159 shape (x and y directions). In order to take into account the buoyancy effects in the mass 160 balance for the gas phase (Eq. 7), the vertical velocity of the gas at the top of the fuel layer $V_{g,z}(\delta)$ has to be described (cf. Fig. 2). This is done from the momentum equation along the 161 vertical axis (Eq. 8). Gas density is defined by using the isobaric perfect gas law (Eq. 9). To 162 163 close the model, the hypothesis of the thermal equilibrium between the gas and solid phases in 164 the fuel layer was set and the gas density was directly obtained from the temperature provided 165 by Eq. (1).

166

167 Numerical implementation

168 Following the assumption of a quasi-static flow, the system of equations was implemented in 169 a simple manner. The characteristic time of the coupled system was assumed to be the one of the energy equation (Simeoni et al. 2003). The 4th order Runge-Kutta method is used to solve 170 171 the equation describing local wind conditions (Butcher 2008). For the thermal balance, a 172 finite difference method was used. An "upwind" difference scheme (finite differences in the 173 direction of flow) was used to take into consideration the extent of convective transfers in the 174 wind direction (Patankar 1980). The resulting system of linear algebraic equations was then 175 solved using the Jacobi iterative method (Sibony and Mardon 1988). The mesh size was of 176 0.01 m while the time step varied from 0.1 s to 0.01 s in order to meet the Courant-177 Friedrichs-Lewy (CFL) condition (Courant et al. 1928). 178 Table 1 shows the value of the model coefficients. They were established for a homogeneous layer of 0.5 kg/m^2 Pinus Pinaster needles with 10 % moisture content 179 180 (Morandini et al. 2005). The model parameters h, K, Q and γ are determined from a measured 181 time-temperature curve obtained for a linear spread under no slope and no wind conditions 182 following the method proposed in Balbi et al. (1999). They are identified once for a given 183 fuel, fuel moisture content and fuel load and remain valid for all the experiments considered 184 hereafter, whatever the slope and wind. The flame length was set to 20 cm that represented the 185 mean experimental height of flame (Morandini et al. 2005). The diffusion coefficient K was 186 decreased by 40 % in comparison with Morandini et al. (2005). Indeed, the energy equation 187 (1) was solved over the whole domain and diffusion losses between fuel cells (at a 188 temperature greater than the ambient temperature) and empty cells (remaining at the ambient 189 temperature) were over-estimated. The K coefficient represents a global diffusion of heat that 190 includes the basic contribution of radiation from the bottom of the flame and from the embers

191 inside the fuel layer (Balbi et al. 1999). To take into account this part of the radiative transfer

and to better account for the long-range radiative transfer from the flame, which is enhanced

for heterogeneous fuels, the radiative coefficient R^* was increased by 20 % in comparison with Morandini et al. (2005).

195 The spreading domain was composed of a homogenous area at the left hand side 196 followed by a heterogeneous zone. The non-homogeneous fuel consisted of combustible and 197 non-combustible square elements randomly distributed with a fixed ratio. The fuel 198 distribution was created with a random number generator. A number between 0 and 1 was 199 attributed to each cell of the domain. Then, each cell with a number lower than the fixed 200 fraction of combustible elements (for instance 0.6 for 60 % of fuel and 40 % of empty space 201 in the domain) was filled with fuel and each cell with a number higher than the ratio was left empty. The neighbourhood influenced by the fire front and the ignition of vegetation were 202 203 directly computed by the model. Each vegetation element was made with a square of four 204 mesh cells. This arbitrary choice was made to allow for both long-range effects of radiation 205 and the critical behaviour of the fire. The tests were performed to assess the model ability to 206 represent real fire behaviour and to consider different possibilities of using fuel heterogeneity 207 both in land management and in fire-fighting.

A straight line ignition was initiated at the left hand side of the domain and the length of the homogeneous zone was set in order to allow a fully developed fire reaching the heterogeneous area. For each condition, the size of the domain was tested to avoid size effects and at least 50 repetitions were completed to obtain mean values of the fire spread properties.

Several numerical test series were conducted under different conditions: slope vs. no slope and wetted vs. dry fuels. As a first approach of the problem, wind configurations were not studied as slope and wind effects were similar for forest fuel beds up to a threshold value (Morandini et al. 2002).

216

217 **Results and discussion**

The simulations presented in the following section were performed to assess the model's ability to represent fire spreading through heterogeneous fuel layers and to discuss the relevance of developing heterogeneous fuel zones for fire fighting and prevention. The different cases studied hereafter include a vegetation pattern made with a mix of Combustible and Non Combustible areas for flat and upslope conditions, a fuel layer made heterogeneous by a mix of dry and wet areas for flat conditions and a combination of the two conditions (Non Combustible areas and wet fuels).

225

226 *Flat conditions*

The first test series was conducted under no slope conditions to evaluate the critical threshold for the fire spread and the effects of heterogeneity on the rate of fire spread. The critical threshold is defined as the status between fire spread success and fire spread stop.

Figure 3 shows the effect of the fraction of combustible elements (FCE) on the rate of fire spread. The threshold was found to be equal to 0.5. It can be seen that near the critical value, the fire rate of spread is almost half the one for the homogeneous fuel (FCE = 1). The rate of spread decreases slowly to the FCE value of 0.52. Then, it decreases steeply to the threshold value of 0.5. This critical behaviour has been observed both in laboratory experiments (Téphany et al. 1997, Nahmias et al. 2000) and in the field (Bradstockl and Gill 1993, Cheney et al. 1993).

The threshold value is lower than the theoretical one found in percolation theory with a Von-Neumann neighbourhood (0.593 for 4 elements with an adjacent side to the considered one) but higher than the theoretical one with a Moore neighbourhood (0.407 for the 8 adjacent elements) (Stauffer 1985). This result implies that the mean neighbourhood for the whole fire front has a configuration between the two previous ones. In the simulations and in real fires, the neighbourhood of a burning element changes with time as it depends on the radiationtransferred ahead of the fire front.

244 To further study the role heterogeneous fuel beds in fire prevention, an area was 245 simulated with two heterogeneous zones (FCE of 0.55 and 0.51). This configuration was 246 chosen because it corresponds to a possible cleaning at the boundaries of a fuelbreak. Figure 4 247 shows a fire spreading in such a configuration. The addition of two zones with FCE over the 248 threshold value (0.5) did not stop the fire as expected but it decreased the rate of spread by 249 35 % in the first zone and by 46 % in the second zone (see table 1). With the heterogeneous 250 domain, the propagation time was increased by around 60 % in comparison with the 251 homogeneous domain. Another interesting effect, shown by Fig. 4 was the decrease in width 252 of the fire front. This effect was systematically observed for all repetitions of the simulations 253 (around 50) and it causes a lower amount of radiation to be sent ahead of the fire front.

254 The effect of the number of burned elements on distance and time was also studied. 255 Percolation theory (Stauffer 1985) and experiments (Beer and Enting 1990, Téphany et al. 256 1997, Namias et al. 2000) show a power-law dependence for this quantity. A similar 257 dependence was obtained with the model but the coefficients were greater than the theoretical 258 ones. This was due to the difference in conditions between the simulations conducted in this 259 work and the percolation studies that consider simple neighbourhoods. Indeed, Téphany et al. 260 (1997) and Nahmias et al. (2000) designed their experiments to match the theoretical 261 neighbouroods; in contrast, the model coefficients were in the same range as those obtained 262 for fire spread under more realistic experimental conditions (Beer and Engins 1990). As there 263 is little data available in literature, this aspect should be further investigated in the form of 264 experiments dedicated to the critical behaviour of forest fires. This objective is clearly beyond 265 the scope of the present paper that is devoted to the evaluation of the relevance of physical 266 modelling to study heterogeneous fuel layers in the context of fire prevention.

267 *Slope conditions*

268 The influence of slope was also analyzed. Figure 5 displays the burned elements at the end of 269 the spreading for a 0.31 FCE and a 10° slope. The upslope direction is shown by an arrow. 270 For this slope, 0.31 FCE was found to be the threshold value. As was seen previously for flat 271 conditions, a slight change in the FCE value (from 0.31 to 0.32) induced a change in the fire 272 regime and demonstrated that the model is able to describe the critical fire behaviour. This 273 value is lower than 0.5 for flat conditions because of the increased heat transfers in the slope 274 direction. Fire fingers developed, as observed in experiments at laboratory scale (Téphany et 275 al. 1997). This behaviour has also been observed for wildfires in heterogeneous areas 276 (Caldarelli et al. 2001), though it must be acknowledge that fire fingers can also be caused by 277 other parameters (changing in wind, uneven ground, infrastructure etc.). The main finger did 278 not reach to the edge of the domain because its width reduced with time (as an effect of the 279 random distribution of empty elements and as the FCE was equal to the critical value).

280 Figure 5 also shows the long-range ignition of combustible elements. In the main 281 spreading direction, the fire front ignited combustible cells even if empty cells were located 282 in between them. This was mainly due to the radiative contribution of the tilted flames in the 283 slope direction as computed by the model. At the sides of the finger, adjacent cells did not burn because the heat transfers were lower. This long-range ignition has been observed in 284 285 laboratory experiments with square elements of wood shavings (Téphany et al. 1997). The 286 authors have also observed it in wildfires but it must be validated by field experiments as the 287 potential causes (radiation or firebrands) are very difficult to separate during uncontrolled 288 fires.

It should be noted that sometimes the combustible cells located at the border of noncombustible zones did not burn (see Figs. 4 and 5) as they were cooled by diffusion losses with the adjacent empty cells. This effect remains to be validated in the field as it is generally observed that continuous pieces of vegetation (with low moisture contents) often burnentirely.

294 Figure 6 shows the temperature distribution at the intermediate time t = 50 s for the 295 same test as depicted in Fig. 5. One can note the end of the spread through the homogeneous 296 zone at the boundaries of the domain (where high temperatures were present). This figure 297 illustrates the long-range radiant effect of the model. The neighbourhood (that is to say the 298 cells that are heated up by the fire front) of the large fire finger in the middle of the domain is 299 very different from the ones of the narrow fingers at the upper and lower parts of the domain. 300 The fuel cells located in front of the large finger are heated 20 cm ahead of the fire front 301 whereas the cells located in front of the small fingers are only heated up to 8 cm. The short-302 range effect for narrow fingers and the long-range effect for large fingers are due to the 303 neighbourhood calculated by the model that varies with the *fire* front shape. This property is 304 not represented by other models based on percolation theory that consider a constant 305 neighborhood for the burning cells, whatever the fire front shape (Ohtsuki and Keyes 1986, 306 Von Niessen and Blumen 1986, Drossel and Schwabl 1992, Zekri et al. 2005). The fire 307 fingers observed in Figs. 5 and 6 correspond to the same effect leading to a narrow fire front 308 in Fig. 4.

309

310 Wetted heterogeneous zones

The last type of fuel heterogeneity considered in this work was that of water. The domain was constituted by a homogeneous fuel with randomly wetted elements. These conditions simulated the random water supply on a fuel bed by spraying. The additional water was assumed to remain outside vegetation. If one considers a fuel cell, the external water acts as a sink source prior to ignition. Thus, a sink term due to the vaporization of vapour at $100^{\circ}C$ is added to Eq. (9) until all the mass of external water has evaporated. Moisture content

317 represents the amount of water inside vegetation and it is indirectly included in the model 318 coefficients h, K, Q and γ (Balbi et al. 1999). Several tests were conducted and an example is 319 depicted in Fig. 7. It represents the arrival of a fire front on a heterogeneous wetted zone with 320 a fraction of wetted elements (FWE) of 0.6. Each of these contained 70 % water, added on the 321 basis of the fuel load (almost dry fuel). When it reached the heterogeneous zone, the fire front 322 dried the cells located just in front of it; for example, the white zone circled in Fig. 7 as an 323 example). Nevertheless, the FWE value was high and it did not allow the fire to propagate. 324 Further simulations were conducted for a lower FWE value (0.5). Even if the fire 325 spread over the whole domain, the decrease in the rate of spread was substantial compared to 326 a homogeneous dry medium (having a 10 % residual moisture content); it spread at half the 327 rate. Furthermore, some unburned areas remained, corresponding to big clusters of wetted 328 elements, as shown in Fig. 8. This phenomenon was observed both in laboratory and field 329 experiments for fuel elements wetted by sprinklers (Nahmias et al. 2000) and for particularly

330 wet vegetation (Santoni et al. 2006).

The configuration used for the simulations is similar in nature as the configuration used by Finney (2003) for fuel mixed with very slow-burning fires. However, neither firefinger nor unburned patched were observed because all fuels burned totally.

The last test evaluated the influence of the moisture content on the threshold value. Heterogeneous areas were considered with wetted vegetation elements and empty elements. A non-spreading configuration was reached with 40 % of water and a 0.4 FCE. As expected, the necessary FCE value that prevented the fire from spreading was low (see the field experiment conducted by Nahmias et al. 2000). Merging the two processes allowed the FCE to be increased substantially to reach the no-spread threshold and it decreased further the spreading time with respect to the dry configuration.

342 About some potential applications

343 Some potential applications of heterogeneous fuels are described in this section and complete 344 the thoughts preented in Nahmias et al. (2000). These potential applications are only the two 345 first authors' perspectives and are a consequence of their joint work in the field and in the 346 laboratory. Obviously, they need to be scientifically studied before any implementation in the 347 field.

Considering land management, the efficiency of fuelbreaks could be increased by heterogeneous areas located on their two sides. This would decrease both the rate of spread of a fire reaching a fuelbreak and the fire front width (as displayed in Fig. 4). The heterogeneous strip on the other side of the fire front arrival would also decrease the probability of ignition by firebrands.

The Wildland-Urban Interface could be treated as heterogeneous buffer zones. The heterogeneity effect could even be increased by using the distribution of Non Combustible Areas in urban development planning such as houses, car parks, roads and so on (Spyratos et al. 2007). A fire reaching these heterogeneous zones would break in several fingers and produce the same benefits as described in this paper for fuel breaks.

Concerning fire-fighting, the technique of putting as much water as possible on the fire front to stop it becomes ineffective under extreme conditions. Figures 7 and 8 show that the fire dynamics is reduced by heterogeneous zones created by randomly wetting the fuel. Heterogeneous areas randomly pre-seeded with water or fire retardant before the arrival of the fire front could create safer conditions for ground fighting and increase wildland/urban interface protection. Sprinklers randomly distributed in the borders of the wildland/urban interface could improve passive fire protection while saving water.

Finally, the combination of random fuel suppression and random wetting before thefire arrival (corresponding to the last case discussed in the previous section) could be used to

367 combine several heterogeneity effects in order to decrease vegetation removal and the
368 associated costs in heterogeneous areas while maintaining a significant effect on the fire.
369

370 Conclusions

371 Different configurations of heterogeneous vegetation have been tested with a physical model.
372 The influence of the heterogeneity of vegetation on the critical behaviour of the fire spread
373 has been studied. The value of the fire spread rate and the evolution of the fire shape have
374 also been examined.

The simulations showed the relevance of using physical modeling to describe fire behaviour in heterogeneous fuels. The model allowed to represent qualitatively the fire behaviour for laboratory and field experiments. Physical models represent an efficient tool to study these problems as they provide many outputs that can be useful for fire-fighting and fire management such as fire shape, rate of fire spread and time for a fire to cross a heterogeneous zone.

A short discussion has been conducted about the potential application of using
 heterogeneous fuels in forest and Wildland-Urban Interface management and protection.

Table 2 presents an overview of the results obtained for the different configurations
used in this study. It was concluded that combining the different processes creating
heterogeneity improves the efficiency of heterogeneous zones.

386 Nevertheless, as there are only few experiments available in literature for
387 heterogeneous fuels, both laboratory and field experiments have to be conducted to test and
388 validate quantitatively the simulation results of physical models.

389

390

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Table 1. Model parameters for a bed of *Pinus pinaster* needles (fuel load of 0.5 kg m^{-2}

 and moisture content of 10 %)

model	h	K	\mathcal{Q}	γ	R^{*}
parameter	(s^{-1})	$(m^2 s^{-1})$	$(m^2 K kg^{-1})$	(s^{-1})	$(K^{-3} s^{-1})$
value	41×10 ⁻³	0.9×10 ⁻⁶	2.34×10^{3}	0.35	2×10 ⁻⁴

Slope	0°	<i>0</i> °	0°	10°	10°	0°
FCE	0.5	0.55 - 0.51	0.31	1	1	0.4
Wetted	No	No	No	70 %	70 %	40 %
elements						
FWE	0	0	0	0.6	0.5	1
Spreading	No	Yes	No	No	Yes	No

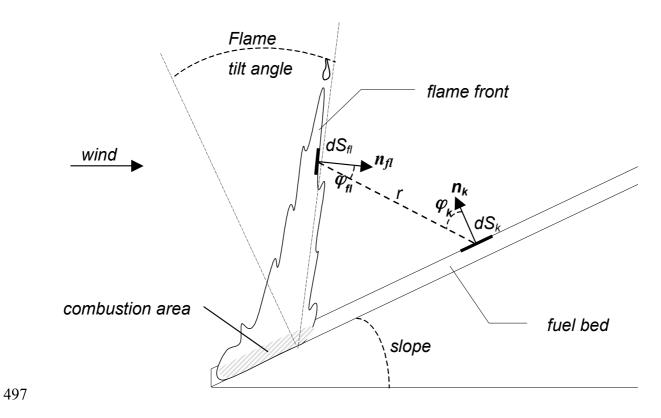


Fig. 1. Radiative transfers between two elementary surfaces of flame and fuel.

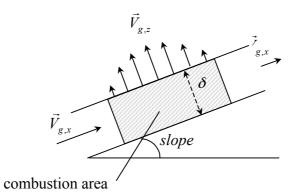


Fig. 2. Schematic representation of the flow within the fuel layer.

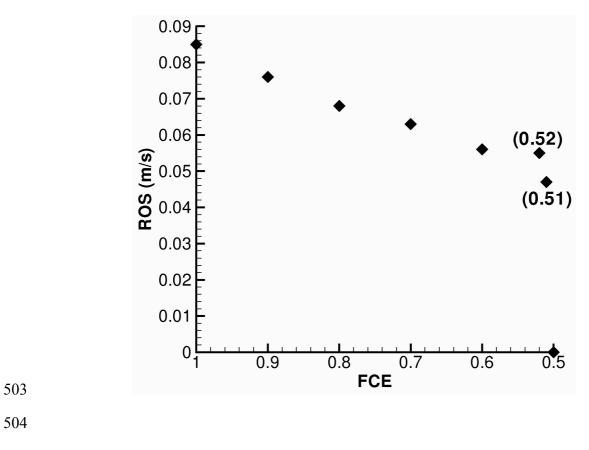
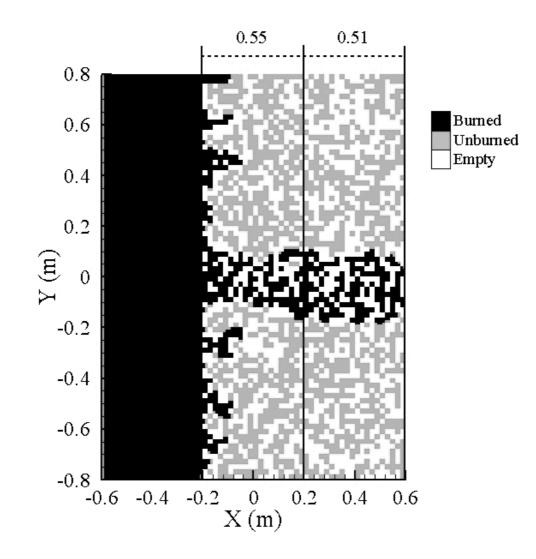


Fig. 3. Rate of fire spread as a function of the FCE for no slope





509 Fig. 4. Burned elements at the end of the spreading for a domain divided in 3 zones:
510 homogeneous, FCE = 0.55 and FCE = 0.51.

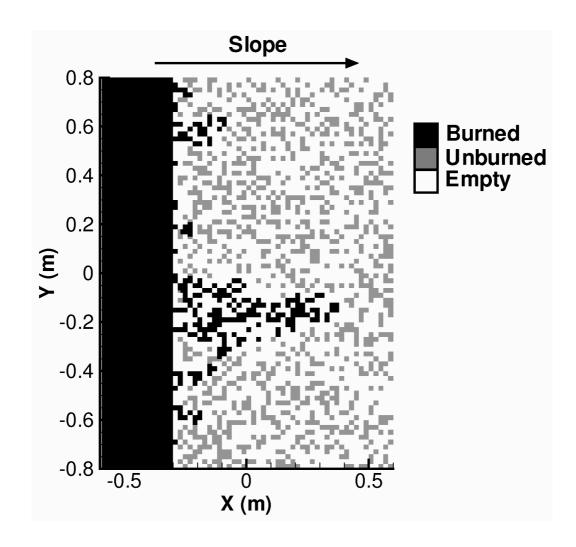
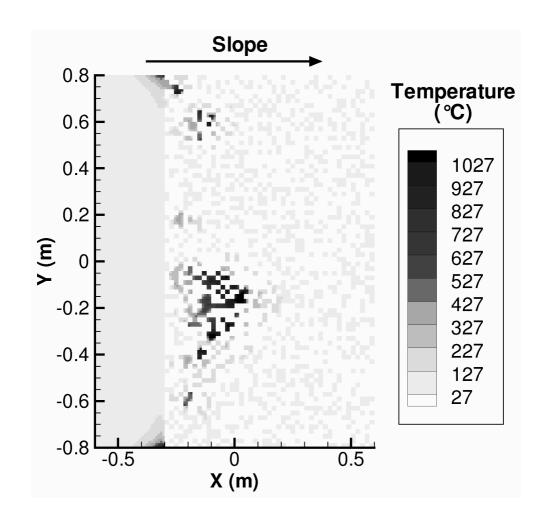




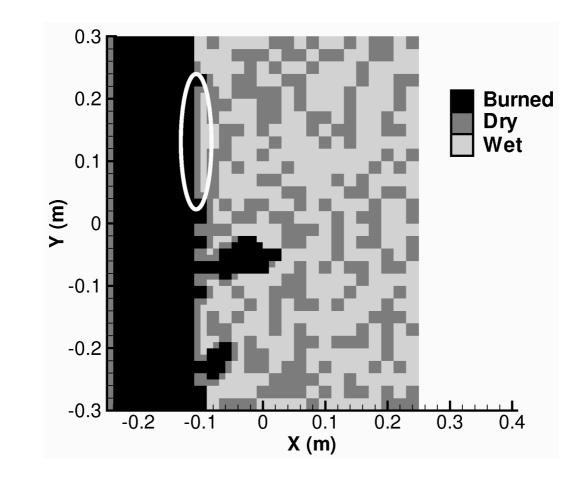


Fig. 5. Burned elements at the end of the spreading for a 0.31 FCE and a 10° slope.



518 Fig. 6. Temperature distribution during the fire spread (t = 50 s) for a 0.31 FCE and a 10°

519 slope.





523 Fig. 7. Burned elements at the end of the spreading for a 0.6 FWE with 70 % of water and524 no slope

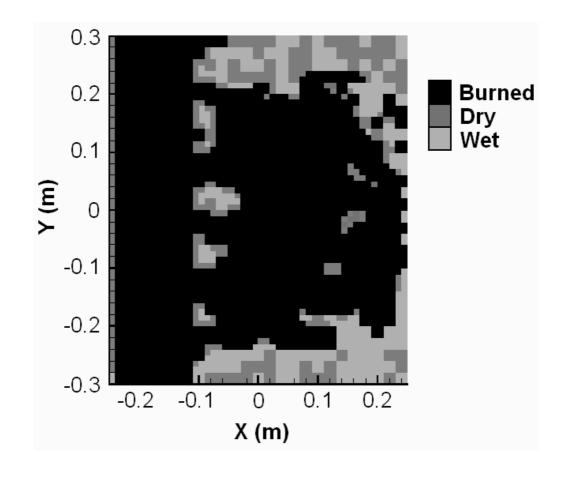


Fig. 8. Burned elements at the end of the spreading for a 0.5 FWE with 70 % of water andno slope.