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Outer-Sphere Coordination Chemistry: Amido-ammonium Ligands as Highly Selective Tetrachloridozinc(II)ate Extractants**

Jennifer R. Turkington, ¹ Violina Cocalia, ²,* Katrina Kendall, ¹ Carole A. Morrison, ¹ Patricia Richardson, ¹ Thomas Sassi, ² Peter A. Tasker, ¹,* Philip J. Bailey ¹,* and Kathryn C. Sole³

[*]Corresponding author; P.T.A. e-mail: peter.tasker@ed.ac.uk; V.C. e-mail: Violina.Cocalia@cytec.com; K.C.S. e-mail: kathysole09@gmail.com

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Supporting information:

Additional figures, tables, and details. This material is available free of charge via the Internet at http://pubs.acs.org

Synopsis

A series of tertiary amines containing one, two, or three amido groups with the atom sequence $R_2N-CH_2-NR'-CO-R''$ are readily protonated, forming six-membered "proton chelates" with a hydrogen bond between the tertiary ammonium N-H+ group and one or two of the pendant amido oxygen atoms. The resulting cations are good outer-sphere ligands for $[ZnCl_4]^{2-}$, forming charge-neutral complexes, $[(LH)_2ZnCl_4]$, and show high selectivity over $[FeCl_4]^-$ and Cl^- as solvent extractants.

Keywords:

Zinc extraction; chloridozinc(II)ate; solvent extraction; supramolecular chemistry; C-H hydrogen bonding; outer-sphere coordination chemistry

^[1]EaStCHEM, School of Chemistry, Joseph Black Building, University of Edinburgh, West Mains Road, Edinburgh, EH9 3JJ, UK.

^[2]Cytec Industries Inc., W. Main St. Stamford, CT 06902, USA.

^[3] Anglo American, Johannesburg, PO Box 106, Crown Mines, S. Africa.

Abstract

Eight new amido functionalised reagents, L¹-L⁸, have been synthesised containing the sequence of atoms R₂N-CH₂-NR'-CO-R'', which upon protonation forms a six-membered chelate with a hydrogen bond between the tertiary ammonium N-H⁺ group and the amido oxygen atom. The mono-cationic ligands, LH⁺, extract tetrachloridometal(II)ates from acidic solutions containing high concentrations of chloride ions via a mechanism in which two ligands address the 'outer sphere' of the [MCl₄]²⁻ unit using both N-H and C-H hydrogen bond donors to form the neutral complex as in $2L + 2HCl + MCl_2 \rightleftharpoons [(LH)_2MCl_4]$. The strengths of L¹-L⁸ as zinc extractants in these pH-dependent equilibria have been shown to be very dependent of the number of amide groups in the R_{3-n}N(CH₂NR'COR'')_n molecules, anti-intuitively decreasing with the number of strong hydrogen bond donors present and following the order monoamides > diamides > triamides. Studies of the effects of chloride concentration on extraction have demonstrated that the monoamides in particular show an unusually high selectivity for [ZnCl₄]² over [FeCl₄] and Cl⁻. Hybrid-DFT calculations on the tri-, diand monoamides, L^2 , L^3 and L^4 , help to rationalise these orders of strength and selectivity. The monoamide L^4 has the most favourable protonation energy because formation of the LH⁺ cation generates a "chelated proton" structure as described above without having to sacrifice an existing intramolecular amide-amide hydrogen bond. The selectivity of extraction of $[ZnCl_4]^{2-}$ over Cl^{-} , represented by the process $2[(LH)Cl] + ZnCl_4^{2-} \rightleftharpoons$ $[(LH)_2ZnCl_4] + 2Cl^2$, is most favourable for L⁴ because it is less effective at binding chloride as it has fewer highly polar N-H hydrogen bond donor groups to interact with this "hard" anion.

Introduction

Recently there has been considerable interest in the use of protonatable organic reagents to recover base metals from acidic chloride media by solvent extraction by forming neutral assemblies such as [(LH)₂MCl₄]. For example, the Falconbridge nickel refinery in Norway uses solvent extraction to separate cobalt and nickel chloridometalates in chloride leach feeds.^{1, 2} Development of such processes has been stimulated by the invention of chloride-resistant materials such as engineered plastics in combination with certain metallic and ceramic components.^{1, 3} However, there are currently no chloride-based hydrometallurgical processes in operation for zinc sulfide ores,⁴ and 80% of the world's zinc is currently produced by the Roast-Leach-Electrowin (RLE) process.^{5, 6} Whilst this is capable of producing high purity zinc, it has a number of drawbacks, particularly the requirement to recover SO₂ from the roasting step and the difficulty of safely disposing the iron residues and red muds or processing them to generate articles of commerce.⁷ Chloride-based extractive hydrometallurgy offers advantages for the concentration and separation metals and can generate elemental sulfur as a by-product.^{8, 9} Oxidative leaching of complex sulfidic ores such as chalcopyrite, see Equations 1-3,^{4, 9-11} is an efficient process as the chlorine needed for oxidation and regenerating lixiviants is produced in downstream electrowinning of the metals. Other advantages include: ambient operating

temperatures, higher solubility of metal values in the pregnant leach solution, low energy consumption in reduction by electrolysis and the generation of higher grade metal at the cathodes.^{3, 8}

$$CuFeS_2 + 3FeCl_3 \rightleftharpoons 4FeCl_2 + CuCl + 2S_{(s)}$$
(1)

$$CuFeS_2 + 3CuCl_2 \rightleftharpoons FeCl_2 + 4CuCl + 2S_{(s)}$$
(2)

$$2\operatorname{CuFeS}_2 + 3\operatorname{Cl}_2 \rightleftharpoons 2\operatorname{FeCl}_2 + 2\operatorname{CuCl} + 4\operatorname{S}_{(s)} \tag{3}$$

The reagents described in this paper are designed to recover ZnCl₄²⁻ from chloride leach streams or spent hydrochloric acid pickling liquors generated by the galvanising industry¹² using 'pH-swing'- controlled solvent extraction processes as in Equation 4.

$$yL_{org} + yH^{+} + MCl_{x}^{y-} \rightleftharpoons [(LH)_{v}MCl_{x}]_{org}$$
(4)

Any such new anion-exchange reagent must show a high *selectivity* for ZnCl₄²⁻ over Cl⁻ to ensure that the reaction in Equation (5) is favoured over that in (6), even at the very high chloride concentrations of the pregnant leach solutions. The chloridozincate binding by the cationic extractant LH⁺ must not be so strong that it prevents water stripping as in Equation (7), and the reagents must show high *selectivity* for Zn(II) over Fe(III) which is usually present in high concentrations in feed streams from oxidative leaching or in pickling liquors (see above). ¹² Ensuring that equilibrium (5) is favoured over (8) is a challenging target because this runs counter to the Hofmeister bias in which more highly charged anions, which have higher hydration energies, are expected to be more difficult to extract into low polarity water-immiscible solvents. ^{13, 14}

$$2L_{\text{org}} + 2H^{+} + ZnCl_{4}^{2-} \rightleftharpoons [(LH)_{2}ZnCl_{4}]_{\text{org}}$$

$$\tag{5}$$

$$L_{\text{org}} + H^{+} + Cl^{-} \rightleftharpoons [(LH)Cl]_{\text{org}}$$
(6)

$$[(LH)_{2}ZnCl_{4}]_{org} + 2H_{2}O \rightleftharpoons 2L_{org} + ZnCl_{2} + 2H_{2}O + 2HCl$$
(7)

$$L_{org} + H^{+} + FeCl_{4}^{-} \rightleftharpoons [(LH)FeCl_{4}]_{org}$$
(8)

Earlier work^{11, 15} has shown that a series of amidopyridines are strong chloridometalate extractants and show a high selectivity for ZnCl₄²⁻ over Cl⁻. They are readily stripped without the pyridine nitrogen atom entering the inner coordination sphere of the metal due to the bulky *t*-butyl substituents in the 6-position (Figure 1a). Protonation of the pyridine nitrogen atom facilitates the formation of a hydrogen bond to the oxygen atom of a pendant amide group (Figure 1a), which in turn pre-organises the ligand, LH⁺, to present several –NH and – CH groups which are polarized to from weakly bonding interactions with the outer-coordination sphere of the chloridometalate.

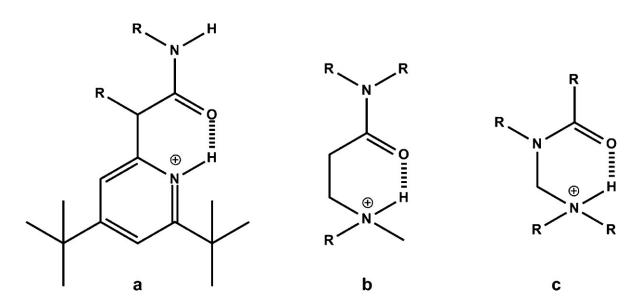


Figure 1. Potential cationic outer-sphere ligands, LH⁺, containing a six-membered 'proton chelate ring'. Aliphatic derivatives of b) have been described previously, ¹¹ and those of the type c) are the subject of this paper.

Outer-sphere complexes formed by the malonamide reagent shown in Figure 2a have been characterised by X-ray crystallography. Nine –CH and –NH bonding interactions are formed between each LH⁺ and a ZnCl₄²⁻ or CoCl₄²⁻ ion in [(LH)₂MCl₄] assemblies. The pyridino 3H and the two amido –NH groups align with the edges of the face of the MCl₄²⁻ ion (see Figure 2), whilst the malonamido –CH bond is directed at the centre of the face. These interactions are reproduced in the energy-minimised structures of [(LH)₂ZnCl₄] obtained through hybrid density functional theory (DFT) calculations. The energy-minimised structure of the chloride salt, [(LH)Cl], is significantly different, with the chloride anion interacting strongly only with the amido –NH groups.¹¹ It appears that the formation of these cyclic *intra*-molecularly hydrogen-bonded structures on protonation presents an array of polarised –CH and –NH units to the outer spheres of large charge-diffuse ions, such as ZnCl₄²⁻, facilitating selectivity of binding over a hard Cl⁻ ion.¹¹

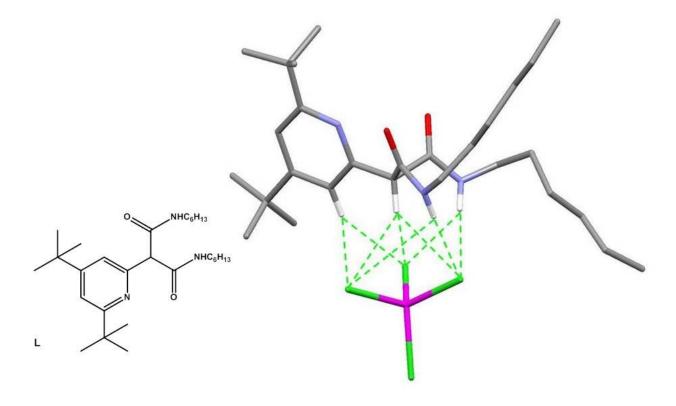


Figure 2. X-ray crystal structure of [(LH)₂ZnCl₄]. The second ligand, LH⁺, has been omitted for clarity.¹⁵

These amidopyridyl reagents are not suitable for commercial operations on cost grounds as their preparation involves the use of air-sensitive *t*-butyllithium. Consequently, a series of reagents based on aliphatic components was developed which contains a similar sequence of atoms which on protonation to give R₂HN⁺-CH₂-CHR-CO-NR₂ will also form six-membered "proton chelates" (Figure 1b). These were shown to display a similarly high strength and selectivity for tetrachloridozincate over chloride to their pyridino analogues and, in some cases, also an unusually high, and potentially useful, selectivity over tetrachloridoferrate(III), FeCl₄⁻. In this paper we test the hypothesis that these beneficial properties arise from the ability to form the six-membered proton chelate by describing the synthesis and properties of a new series of reagents (L¹-L⁸, Figure 3) which could also form the chelate (Figure 1c), but using a different atom sequence in the ligand, R₂HN⁺-CH₂-NR-CO-R. The new reagents, L¹-L⁸, were designed to allow us to probe how the strength of chloridometalate extractants depends on the number of pendant amide groups present. As these are all secondary amide groups which provide strong H-bond donors, it was initially assumed that increasing their number would favour ZnCl₄²⁻ uptake. These extractants are compared to triethylhexylamine (TEHA), which has been used as a model for the Alamine® reagents.

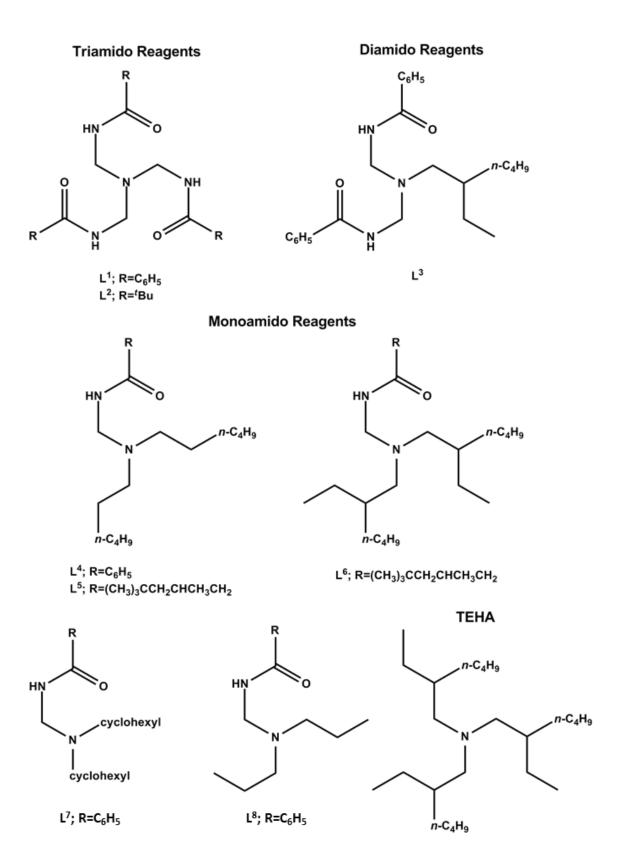


Figure 3. Ligand Series 3, L¹-L⁸, and the aliphatic amine benchmark (TEHA).

Experimental

Solvents and reagents were sourced from Aldrich, Alfa Aesar, Fisher or Acros and de-ionised water was obtained from a Milli-Q purification system. ^{1}H and ^{13}C nuclear magnetic resonance (NMR) spectra were obtained on a Bruker AVA 400 or 500 spectrometer as solutions in CDCl₃ or DMSO- $_{d6}$. Chemical shifts (δ) are reported in parts per million (ppm) relative to the residual solvent (δ_{H} 7.26 and δ_{C} 77.0 or δ_{H} 2.50 and δ_{C} 39.5). Electrospray (ES) mass spectra were recorded on a VG Autospec instrument. It was not possible to obtain reliable CHN analysis of the extractants which were obtained as oils.

Benzamidomethyltriethylammonium chloride ¹⁶⁻¹⁸: Thionyl chloride (50 mL, 0.69 mol), was added dropwise to a suspension of N-(hydroxymethyl)benzamide (35.9 g, 0.23 mol) in molecular sieve-dried dichloromethane (250 mL) under nitrogen. The resulting clear solution was poured onto heptanes (500 mL) and the fine colorless precipitate which formed was filtered and washed with a further portion of heptanes (50 mL). Due to the moisture-sensitive nature of this material the N-(chloromethyl)benzamide (30.1 g, 0.18 mol) was immediately dissolved in molecular sieve-dried acetone (150 mL) and added to a solution of triethylamine (31.0 mL, 0.22 mol) in dry acetone (250 mL) in one portion. A further 200 mL of acetone was added to the resulting thick white suspension. After stirring for 30 mins the mixture was filtered under vacuum yielding a colorless powder which, after washing with acetone, was recrystallised from chloroform to give benzamidomethyltriethyl chloride as white crystals. Yield = 37.00 g (77%); ${}^{1}H$ NMR (δ_{H} , 400 MHz, DMSO-_{d6}) 1.2 (t, 9H, NCH₂CH₃), 3.2 (q, 6H, NCH₂CH₃), 4.7 (d, 2H, NCH₂NH), 7.5 (t, 2H, COCCHCHCHCHCH-aromatic), 7.6 (t, 1H, COCCHCHCHCHCH-aromatic) 8.0 (d, 2H, COCCHCHCHCHCH-aromatic), 9.7 (t, 1H, -NH); 13 C NMR ($\delta_{\rm C}$, 400 MHz, DMSO- $_{d6}$) 7.86 (3C, -[CH₂CH₃]₃), 50.61 (3C, -N[CH₂CH₃]₃), 61.30 (1C, aromatic), 128.69 (2C, aromatic) 128.90 (2C, aromatic), 132.99 (1C, NCH₂N), 133.06 (1C, aromatic), 169.09 (1C, -CO); m/z (ESI) 235 [M]⁺; Anal. Calcd. for C₁₄H₂₃CIN₂O: C 62.09, H 8.56, N 10.34. Found: C 62.03, H 8.55, N 10.49.

Hydroxyltrimethylacetamide¹⁹⁻²¹: Trimethylacetamide (11.46 g, 0.112 mol) and potassium hydroxide (0.66 g, 0.016 mol) were dissolved in 37% formalin (8 mL, 0.08 mol). The mixture was stirred at 70°C for 5 mins, then left to stir at room temperature for 16 h. The solution was then acidified to pH 7 (by litmus) using 6 M hydrochloric acid. The solution was then concentrated *in vacuo*. The residue was dissolved into acetone and dried over magnesium sulfate, which was then removed by filtration. Further concentration *in vacuo* of the filtrate to remove acetone afforded the product as a solid. Yield = 12.23 g (83%); ¹H NMR (δ_H, 400 MHz, CDCl₃) 1.2 (s, 9H, C(CH₃)₃), 4.7 (d, 2H, HOCH₂NH), 6.7 (s_{broad}, 1H, NH); ¹³C NMR (δ_C, 400 MHz, CDCl₃) 27.3 (3C, C(CH₃)₃), 38.7 (1C, C(CH₃)₃), 64.8 (1C, HOCH₂NH), 180.4 (1C, CO); m/z (EI) 131.1 [M]⁺.

N-tert-butylformamidomethyltriethylammonium chloride^{16, 17, 22}: To a stirred suspension of hydroxyltrimethylacetamide (5.95 g, 0.017 mol) in 60 mL dry dichloromethane under nitrogen, thionyl chloride (10.55 mL, 0.145 mol) was added dropwise. Heptane (200 mL) was added to the stirring mixture, affording an oil. Rapidly the acyltrimethylacetamide oil was separated and dissolved in dry acetone (30 mL).

The whole solution was added at once to a vigorously stirring mixture of triethylamine (8.71 mL, 0.062 mol) in dry acetone (60 mL). Additional dry acetone (40 mL) was added and the mixture stirred for 30 mins at room temperature. The solution was then filtered *in vacuo*. The filtrate was then concentrated *in vacuo*, affording the product as an oil. Yield = 7.34 g (74%). ¹H NMR (δ_H , 400 MHz, CDCl₃) 1.35 (s, 9H, CC \underline{H}_3)₃), 1.47 (t, 9H, N(CH₂)₃(C \underline{H}_3)₃), 3.30 (q, 6H, N(C \underline{H}_2)₃(CH₃)₃), 4.82 (d, 2H, NC \underline{H}_2 NH), 6.8 (s_{broad}, 1H, N \underline{H}); ¹³C NMR (δ_C , 400 MHz, CDCl₃) 27.3 (3C, (C \underline{C} H₃)₃), 39.5 (1C, \underline{C} (CH₃)₃), 45.8 (3C, N(CH₂)₃(\underline{C} H₃)₃), 51.6 (1C, N \underline{C} H₂NH), 62.7 (3C, N(\underline{C} H₂)₃(CH₃)₃), 182.5 (1C, CO); m/z (ESI) 215.48 [M-Cl]⁺.

3,5,5-trimethylhexanamide: To a round-bottom flask containing aqueous ammonia (35%, 80 mL, 1.076 mol) cooled to 0°C, 3,5,5-trimethylhexanoyl chloride (14.40 g, 0.082 mol) was added dropwise. The reaction mixture was kept at 0°C for 20 mins, then warmed to room temperature and stirred for 3 hours. The product was extracted into dichloromethane, washed with distilled water and dried over magnesium sulfate, then concentrated *in vacuo* to yield a colorless solid. Yield = 9.64 g (75%); 1 H NMR (δ_{H} , 400 MHz, CDCl₃) 0.94 (s, 9H, CHCH₂C(CH₃)₃), 1.03 (d, 3H, CCH₂CHCH₃), 1.2 (m, 2H, CCH₂CHCH₂), 2.0 (m, 1H, CCH₂CH), 1.95-2.18 (ddd, 2H, CCH₂CH), 5.48 (s, 2H, CNH₂); 13 C NMR (δ_{C} , 400 MHz, CDCl₃) 22.56 (1C, C(CH₃)₃), 27.32 (1C, CHCH₂C), 30.01 (3C, C(CH₃)₃), 31.06 (1C, CHCH₂C), 45.87 (1C, CHCH₃), 50.72 (1C, COCH₂CH), 175.1 (1C, CO); m/z (ESI) 157.7 [M]⁺.

Tris[*N*-**phenylformamidomethyl]amine** (L^1)^{23, 24}: Aqueous ammonia (35%, 0.61 mL, 0.12 mol) was added dropwise to a stirred solution of benzamidomethyltriethylammonium chloride (10.0 g, 0.04 mol) dissolved in the minimum amount of distilled water (200 mL). The colorless precipitate which separated immediately was filtered after stirring for a further 30 mins and was recrystallised from acetone by slow evaporation to yield colorless crystals of tris[*N*-phenylformamidomethyl]amine. Yield = 2.06 g (54%); ¹H NMR (δ_H, 400 MHz, CDCl₃) 4.6 (d, 6H, NC<u>H</u>₂NH), 7.2 (t, 6H, COCCHC<u>H</u>CHCHCH-_{aromatic}), 7.3 (t, 3H, COCCHCHCHCHCH-_{aromatic}), 7.5 (d, 6H, COCCHCHCHCHCHCH-_{aromatic}), 8.0 (t, 3H, N<u>H</u>); ¹³C NMR (δ_C, 400 MHz, CDCl₃) 57.97 (3C, NCH₂N), 126.93 (6C, aromatic), 128.24 (6C, aromatic), 131.55 (3C, aromatic), 133.51 (3C, aromatic), 168.75 (3C, CO); m/z (ESI) 439 [M+Na⁺]⁺; *Anal. Calcd.* for C₂₄H₂₄N₄O₃: C 69.21, H 5.81, 13.45. *Found*: C 68.28, H 5.76, N 13.12.

Tris[N-tert-butylformamidomethyl]amine (L^2)^{19-21, 23, 24}: To a solution of N-tert-

butylformamidomethltriethylammonium chloride (2.87 g, 0.011 mol) in distilled water (16 mL) was added a mixture of 35% ammonia solution (0.16 mL, 2.9×10^{-3} mol) and triethylamine (0.3 mL, 2.2×10^{-3} mol) in distilled water (9 mL). The reaction mixture was stirred for 30 mins at room temperature. The precipitate was filtered off *in vacuo*, and dissolved in chloroform and washed with distilled water (25 mL). The organic layer was dried over magnesium sulfate and the chloroform removed *in vacuo*, to afford the product as a solid. Yield = 0.36 g (9%); ¹H NMR (δ_H , 400 MHz, CDCl₃) 1.2 (s, 27H, C(CH₃)₃), 4.2 (d, 6H, NCH₂NH), 7.0 (s, 3H, NH); ¹³C NMR (δ_C , 400 MHz, CDCl₃) 27.6 (9C, C(CH₃)₃), 38.8 (3C, C(CH₃)₃), 55.3 (3C, NCH₂NH), 180.4

 $(3C, \underline{CO})$; m/z (EI) 356.3 [M]⁺; Anal. Calcd. for $C_{18}H_{36}N_4O_3$: C 60.64, H 10.18, N 15.72. Found: C 60.58, H 10.15, N 15.64.

N-[(2-ethylhexyl)](phenylformamido)methyl]amino]methyl benzamide (L³): A solution of 2-ethylhexylamine (0.60 g, 4.6x10⁻³ mol) and triethylamine (0.14 mL, 1.0x10⁻³ mol) in distilled water (5 mL) was added to a stirred suspension of benzamidomethyltriethylammonium chloride (2.53 g, 9.4x10⁻³ mol) in distilled water (10 mL). After 30 mins the product was extracted into diethyl ether (4 x 5 mL), dried over magnesium sulfate and concentrated *in vacuo*. The resulting golden oil was purified by flash column chromatography (silica, 1:1 ethyl acetate/hexane). Yield = 1.95 g (54%); ¹H NMR (δ_H, 400 MHz, CDCl₃) 0.8 - 2 (15H, alkyl), 2.55 (d, 2H, NCH₂C), 4.5 (d, 4H, (NHCH₂N)₂), 7.4 (t, 2H, (NHCH₂N)₂), 7.6 (m, 6H, (COCCHCHCHCHCH₂), 7.9 (d, 4H, (COCCHCHCHCH₂); ¹³C NMR (δ_c, 400 MHz, CDCl₃) 10.60 (1C, CH₂CH₂CH₃), 14.16 (1C, CHCH₂CH₃), 23.23 (1C, alkyl), 24.09 (1C, alkyl), 28.32 (1C, alkyl), 31.02 (1C, alkyl), 36.66 (1C, CH₂CHCH₂), 52.66 (1C, NCH₂C), 57.17 (2C, (NCH₂N)₂), 127.10 (4C, aromatic), 128.62 (4C, aromatic), 131.73 (2C, aromatic), 134.06 (2C, CCON), 168.49 (2C, NCO); m/z (ESI) 396 [M+H]⁺.

N-[(di-*n*-hexylamino)methyl]benzamide (L⁴)²³⁻²⁵: To a rapidly stirring slurry of (benzamidomethyl)triethylammonium chloride (2.45 g, 9.0x10⁻³ mol) in tetrahydrofuran (60 mL), dihexylamine (2.09 mL, 9.0x10⁻³ mol) was added in one portion and heated to reflux for 45 mins, then concentrated *in vacuo*. The reaction mixture was re-dissolved in dichloromethane (50 mL) and washed with 2 x 50 mL portions of saturated sodium carbonate solution. The organic layer was dried over magnesium sulfate then concentrated *in vacuo* and the resulting golden oil was purified by flash column chromatography (silica, 9:1 dichloromethane/methanol). Yield = 1.16 g (41%); ¹H NMR (δ_H, 400 MHz, CDCl₃) 0.89 (t, 6H, (CH₂CH₂CH₃)₂), 1.29 (m, 12H, (CH₂CH₂CH₂CH₃)₂), 1.53 (m, 4H, N(CH₂CH₂CH₂)₂, 2.55 (t, 4H, N(CH₂CH₂CH₂)₂), 4.41 (d, 2H, NHCH₂N), 6.60 (t, 1H, NHCH₂N), 7.42 (t, 2H, COCCHCHCHCHCH), 7.49 (m, 1H, COCCHCHCHCHCH), 7.79 (m, 2H, COCCHCHCHCHCHCH); ¹³C NMR (δ_C, 400 MHz, CDCl₃); 14.06 (2C, alkyl), 22.67 (2C, alkyl), 27.15 (2C, alkyl), 27.66 (2C, alkyl), 31.76 (2C, alkyl), 52.14 (2C, alkyl), 58.77 (1C, alkyl), 126.94 (2C, aromatic), 128.54 (2C, aromatic), 131.46 (1C, aromatic), 134.69 (1C, aromatic), 167.92 (1C, CO); m/z (ESI) 319 [M+H]⁺.

N-[bis(2-ethylhexyl)amino]methyl-3,5,5-trimethylhexanamide (L^6)²⁶: In a round-bottom flask 3,5,5trimethylhexanamide $(2.00 \text{ g}, 1.3 \times 10^{-3} \text{ mol})$ was dissolved in the minimum amount of methanol and cooled to 0°C. To this, formaldehyde (1.031 g, 1.3x10⁻³ mol) and di-2-ethylhexylamine (3.067 g, 1.3x10⁻³ mol) were added. The reaction was warmed to 40°C and allowed to stir for 6 days at this temperature. After this time the reaction mixture was concentrated in vacuo and the resulting golden oil was purified by flash column chromatography (silica, 99:1:0.1 dichloromethane/methanol/aqueous ammonia (35%)). Yield = 2.78 g (57%); ¹H NMR (δ_H, 400 MHz, CDCl₃) 0.84 (t, 4H, N(CH₂CHCH₂CH₂CH₂CH₂CH₂CH₃)₂), 0.88 (m, 4H, N(CH₂CH)₂), 0.93 (d, 6H, N(CH₂CHCH₂CH₃CH₂CH₂CH₂CH₃)₂), 0.99 (m, 3H, COCH₂CHCH₃), 1.14-1.36 (m, 1H, COCH₂CHCH₃), 1.27 (m, 27H, N(CH₂CHCH₂CH₂CH₃CH₂CH₂CH₃)₂ and COCH₂CHCH₂C(CH₃)₃), 1.92-2.21 (dq, 2H, N(CH₂CH_CH₂CH₃)₂), 2.25 (dd, 4H, NHCOCH₂CHCH₂), 4.15 (d, 2H, NHCH₂N), 5.61 (t, 1H, NH); 13 C NMR (δ_{C} , 400 MHz, CDCl₃) 10.71 (1C, CH₂C(CH₃)₃), 14.13 (3C, CH₂C(CH₃)₃), 22.59 (2C, N(CH₂CHCH₂CH₂CH₃)₂), 23.22 (2C, N(CH₂CHCH₂CH₂CH₂CH₃)₂), 24.25 (2C, N(CH₂CHCH₂CH₂CH₃)₂), 27.27 (1C, COCH₂CH<u>C</u>H₂), 28.97 (2C, N(CH₂CHCH₂<u>C</u>H₃)₂), 30.05 (2C, N(CH₂CH_CH₂CH₃)₂), 31.11 (2C, -N(CH₂CHCH₂CH₃)₂), 37.21 (2C, N(CH₂)₂), 37.22 (2C, alkyl), 46.97 (1C, CHCH₃), 50.74 (1C, COCH₂CH), 57.04 (1C, COCH₂CH), 58.60 (1C, NHCH₂N), 172.68 (1C, CO); m/z (ESI) 422 [M+H]⁺.

N-[(di-*n*-cyclohexylamino)methyl]benzamide (L⁷)²³⁻²⁵: To a rapidly stirring slurry of (benzamidomethyl)triethylammonium chloride (4.00 g, 0.015 mol) in tetrahydrofuran (60 mL), di-*n*-cyclohexylamine (3.28 mL, 0.016 mol) was added in one portion and allowed to heat at 70°C for 45 mins, then concentrated *in vacuo*. The mixture was then redissolved in dichloromethane (50 mL) and washed with 4 x 50 mL portions of saturated sodium carbonate solution. The organic layer was dried over magnesium sulfate then concentrated *in vacuo* and purified by trituration with diethylether to yield a colorless solid. Yield = 4.65 g (55%); ¹H NMR (δ_H, 500 MHz, CDCl₃) 1.1 (m, 2H, NCHCH₂CH₂CH₂H₄H_b), 1.3 (m, 8H, NCHCH₂CH₂), 1.6 (d, 2H, NCHCH₂CH₂CH₄H_b), 1.8 (m, 8H, NCHCH₂CH₂), 2.7 (m, 2H, NCH), 4.5 (d, 2H, NCH₂NH), 6.0 (s, 1H, NH), 7.4 (t, 2H, COCCHCHCHCHCH-_{aromatic}), 7.5 (t, 1H, COCCHCHCHCHCH-_{aromatic}), 7.8 (d, 2H, COCCHCHCHCHCHCH_{-aromatic}); ¹³C NMR (δ_C, 400 MHz, CDCl₃) 25.98 (2C, (*cy*-C₆H₁₁)₂), 26.29 (4C, (*cy*-C₆H₁₁)₂), 32.88 (4C, (*cy*-C₆H₁₁)₂), 54.84 (2C, (*cy*-C₆H₁₁)₂), 58.60 (1C, NCH₂-N), 126.79 (2C, aromatic), 128.55 (2C, aromatic), 131.25 (1C, aromatic), 135. 00 (1C, aromatic), 166.69 (1C, CO); m/z (ESI) 314.2 [M]⁺; *Anal. Calcd.* for C₂₀H₃₀N₂O: C 76.39, H 9.62, N 8.91. *Found*: C 75.35, H 9.34, N 8.80.

N-[di-*n*-propylamino methyl] benzamide $(L^8)^{23-25}$: A stirred suspension of

(benzamidomethyl)triethylammonium chloride (2.5 g, 9.3×10^{-3} mol) in distilled water (60 mL) was heated until dissolved. To this solution di-*n*-propylamine (1.51 mL, 1.0×10^{-3} mol) was added in one portion and allowed to stir for 30 mins. The resultant colorless precipitate was collected by vacuum filtration. Yield = 1.35 g (57%); 1 H NMR (δ_{H} , 400 MHz, CDCl₃) 0.9 (t, 6H, N(CH₂CH₂CH₃)₂), 1.6 (m, 4H, N(CH₂CH₂)₂), 2.5 (t, 4H, N(CH₂CH₂)₂), 4.4 (d, 2H, NCH₂NH), 6.4 (t, 1H, NH), 7.4 (t, 2H, COCCHCHCHCHCH-aromatic), 7.5 (t, 1H, COCCHCHCHCHCHCH-aromatic), 7.8 (d, 2H, COCCHCHCHCHCH-aromatic); 13 C NMR (δ_{C} , 400 MHz, CDCl₃) 11.91 (2C, NCH₂CH₂CH₃), 20.94 (2C, NCH₂CH₂CH₃), 54.17 (2C, NCH₂CH₂CH₃), 58.90 (1C, N-CH₂-N), 126.90 (2C, aromatic), 128.62 (2C, aromatic), 131.51 (1C, aromatic), 134. 72 (1C, aromatic), 167.82 (1C, CO); m/z (ESI) 234 [M+H]⁺.

General Extraction Procedures: Analytical-grade toluene was used as the water-immiscible solvent for the extractants and deionised water for the metal chloride solutions. Inductively coupled plasma optical emission spectroscopy (ICP-OES) calibration standards for zinc were prepared by dilution of commercially available standards from Aldrich. Extractions were performed by vigorously stirring solutions with magnetic stir bars in sealed vials for 1 hour at room temperature. All volumes were measured by using 1 and 5 mL Rainin edp3 automatic pipettes. ICP-OES was carried out on a Perkin Elmer Optima 5300 DV, employing an radio frequency (RF) forward power of 1400 W, with argon gas flows of 15, 0.2 and 0.75 L min⁻¹ for plasma, auxiliary, and nebuliser flows, respectively. Using a peristaltic pump, sample solutions were taken up into a Gem Tip cross-Flow nebuliser and Scotts spray chamber at a rate of 1.50 mL min⁻¹.

Dependence of Zn(II) loading on pH: A series of aqueous solutions of ZnCl₂ (0.01 M) were prepared by adding 2.5 mL of ZnCl₂ solution (0.02 M ZnCl₂ in 6 M LiCl) to variable volumes of HCl solution (6 M or 0.1 M) and making up to 5 mL with 6 M LiCl solution. These solutions, with pH ranging between -2 < pH < 6, were contacted with an equal volume of 0.01 M extractant solution in toluene and stirred at room temperature. After one hour the phases were allowed to separate and a 1 mL aliquot of the organic phase was transferred to a 10 mL volumetric flask, the toluene was removed by evaporation *in vacuo* and the flask made up to the mark with butan-1-ol for ICP-OES analysis. The equilibrium pH of the aqueous phase was recorded using a pH meter.

Dependence of Zn(II) loading on ligand concentration: Solutions of extractants were prepared at concentrations ranging between 0.004 – 0.01 M by adding aliquots of a 0.05 M solution in toluene to a 5 mL volumetric flask and making up to the mark with toluene. These extractant solutions were contacted with 5 mL of chloridometalate solution (0.003 M, 6 M LiCl, 0.1 M H⁺) and stirring for one hour, after which time, the phases were separated and 1 mL aliquots of both the aqueous and the organic phases were reduced to dryness and then made up to 10 mL with butan-1-ol for ICP-OES analysis.

<u>Dependence of Zn(II) or Fe(III) loading on chloride concentration:</u> A series of aqueous chloridozincate solutions (0.01 M ZnCl₂, 0.1 M H⁺) with varying chloride concentration ranging between 0.1 M and 6 M were

prepared by adding 0.0625 mL of MCl₂ solution (0.8 M ZnCl₂ or FeCl₃ in 6 M HCl) to varying volumes of 6 M LiCl solution and making up to 5 mL with deionised water. These metal chloride solutions were contacted with an equal volume of 0.01 M extractant solution in toluene and allowed to stir at room temperature. After one hour, 1 mL aliquots of the organic phase were transferred to a 10 mL volumetric flask, the toluene removed by evaporation *in vacuo* and the residue made up to the mark with butan-1-ol for ICP-OES analysis.

General Chloride Analysis Procedure²⁷: A 1 mL sample of the loaded organic phase was passed through phase separation paper to remove any entrained aqueous phase before contacting with 2 mL of 0.1 M NaOH. After stirring for 1 hour, the phases were separated and 100 μL of the resulting aqueous phase was diluted to 1 mL and analysed using ion chromatography which was performed on a Dionex ICS-1100 system running a 45 μM CO₃²⁻/14 μM HCO₃⁻ eluent. Detection and determination of the concentrations of ions used the suppressed conductivity method. The system is equipped with a DS6 conductivity cell, an ASRS 300 suppressor unit, a thermal compartment housing a Dionex IonPac AG22 (4 mm x 50 mm) guard column and a Dionex ionPac AS22 (4 mm x 250 mm) analytical column. 25 μL samples were injected and the flow rate was set at 1.2 mL min⁻¹. The column temperature maintained at 30°C throughout. The Chromeleon 6.8 software supplied by Dionex was used for data collection and processing.

General Method for Calculating Selectivity: At high $[H^+]$ and $[Cl^-]$ concentrations if not all of the ligand forms a complex with $ZnCl_4^{2-}$, it was assumed that the remainder is in the form of its hydrochloric salt, [(LH)Cl]. This situation is represented by the competition between chloridozincate and chloride for the ligand which is shown in Equation (9). The selectivity for chloridozincate is defined by Equation (10), in which K is the equilibrium constant for the process in Equation 9.

$$[(LH)_{2}ZnCl_{4}]_{org} + 2Cl^{-} \rightleftharpoons [ZnCl_{4}]^{2-} + 2[(LH)Cl]_{org}$$
(9)

Selectivity
$$\propto \frac{1}{K} = \frac{[(LH)_2 ZnCl_4][Cl^-]^2}{[ZnCl_4^2][(LH)Cl]^2}$$
 (10)

General Procedure for Calculating logD: Extractions were prepared with varying concentrations of ligand and contacted with a known excess of zinc solution. The 0.1 M zinc solutions were prepared with 6 M HCl in order to ensure formation of the ZnCl₄²⁻ species. After stirring for 30 mins the aqueous and organic phases were separated, 1 mL samples were taken, reduced *in vacuo* and diluted to 10 mL with butan-1-ol for ICP-OES analysis. The determined zinc concentrations were used to calculate the distribution coefficient for zinc using Equation 11:

$$D = \frac{[zinc]_{org}}{[zinc]_{aq}}$$
 (11)

General Procedure for Preparing NMR Samples: 0.01 M ligand solutions in toluene were contacted with a 6 M HCl and 6 M [Cl] solution of ZnCl₂. After rapidly stirring for 1 hour, the phases were separated and a 2 mL sample of the organic phase was concentrated *in vacuo* and dissolved in deuterated toluene for NMR analysis.

Computational Modelling Analysis: Calculations were carried out at B3LYP/6-31G (d,p) using the Gaussian 09 program. The hybrid DFT level of theory was chosen as it adequately models the complexes in question where the dominant interactions are electrostatic and charge transfer in nature. Geometry optimisations were carried out to determine the preferred conformation, which were then pursued by analytical frequency calculations to confirm that the conformations obtained correspond to minima on the potential energy surface. The energies of the energy-minimised structures of the extractants (L), ligands (LH⁺) and the [(LH)₂ZnCl₄], [(LH)Cl] and [(LH)FeCl₄] complexes were used to calculate the formation enthalpies (FEs, the enthalpies associated with the processes in equations 12, 13 and 14).

$$2L + 2H_3O^+ + ZnCl_4^{2-} \rightleftharpoons [(LH)_2ZnCl_4] + 2H_2O$$
 (12) $L + H_3O^+ + Cl^- \rightleftharpoons [LHCl] + H_2O$ (13) $L + H_3O^+ + FeCl_4^- \rightleftharpoons [(LH)FeCl_4] + H_2O$ (14)

Proton affinities (PAs)³⁰ were calculated for equation 15 using the terms listed in equation 16.

$$L + H_3O^+ \rightleftharpoons LH^+ + H_2O$$

$$[LH^+(E_{tot}) + H_2O(E_{tot})] - [L(E_{tot}) + H_3O^+(E_{tot})]$$
(15) PA =

The binding energies (*BE*s) in the complexes are defined as the energy released in bringing together the preformed cations, LH⁺, with the metalate anion (or the chloride anion) in the gas phase to generate the energy-minimised form of the complex, in accordance with equation 17;

$$BE = [complex(E_{tot})] - [LH^{+}(E_{tot}) + anion(E_{tot})] + BSSE + \Delta nRT$$
(17)

where the total energy of each species, *i.e.*, the E_{tot} term (also known as the enthalpy), is made up of the sum of the electronic (E_{el}), vibrational (E_{vib}), rotational (E_{rot}) and translational (E_{trans}) energies;

$$E_{\text{tot}} = E_{\text{el}} + E_{\text{vib}} + E_{\text{rot}} + E_{\text{trans}}$$
 (18)

Calculation of these terms is performed automatically by Gaussian 09 once the vibrational frequencies are known. As is standard in electronic structure calculations, E_{el} is assumed to be zero, where E_{el} corresponds to the contribution to the total energy from the first excited state. E_{vib} is obtained by simply adding up the ½ $\hbar\omega$ contribution from each vibrational mode, ω . The rotational and translational energy values are modelled as a continuum, in accordance with classical equipartition theory, which equates to 3/2RT for each. Δn is a constant that accounts for the change in the number of species during the reaction, *i.e.*, $\Delta n = -2$ for (12) and $\Delta n = -1$ for (13) and (14). A correction factor for basis set superposition error (BSSE) has also been included which is determined using the counterpoise method of Boys and Bernardi. Finally, the unit operations of protonation and anion binding are combined to yield the formation enthalpy which accounts for the overall process, giving an overall formation enthalpy (FE) equation of:

$$FE = [complex(E_{tot}) + xH_2O(E_{tot})] - [xL(E_{tot}) + anion(E_{tot}) + xH_3O^{\dagger}(E_{tot})] + BSSE + \Delta nRT$$
(19)

Further calculations were then performed on the optimised structures, in order to rationalise the properties of the individual hydrogen bond interactions found. This was done using natural bond orbital (NBO) analysis, which describes hydrogen bonding interactions within a framework of donor (i) –acceptor (j) charge-transfer interactions between idealised 'Lewis'-type orbitals. The energetics of each interaction are estimated using a second-order perturbative approach equation (20).

$$E(2) = \Delta E_{ij} = q_i \frac{F(i, j)^2}{\varepsilon_j - \varepsilon_i}$$
(20)

In this equation, q_i is the donor orbital occupancy, ε_i and ε_j are the orbital energies and F(i,j) is the off-diagonal NBO Fock matrix element.³²

Results and Discussion

A common precursor, benzamidomethyltriethylammonium chloride (1), was used to prepare the ligands L^1 , L^3 and $L^{4,7,8}$ by reaction with ammonia, 2-ethylhexylamine and the appropriate secondary amine respectively

as outlined in Scheme 1. Three equivalents of thionyl chloride were used in the first step in order to ensure completion of the reaction.

$$C_{6}H_{5}$$

$$C_{7}H_{7}$$

$$C_{7}H_{7}$$

$$C_{8}H_{7}$$

$$C_{$$

Scheme 1. Synthesis of tri-, di- and monoamido functionalised amine extractants L^1 , L^3 , L^4 , L^7 and L^8 . Reagents & conditions: (i) dichloromethane, $N_{2(g)}$, room temperature, (ii) acetone, room temperature, (iii) distilled water, triethylamine, room temperature, (iv) distilled water, room temperature, (v) tetrahydrofuran, reflux. $^{16-18, 23-25}$

Of these, only L³ and L⁴ showed sufficient solubility in toluene in both the neutral and protonated forms to carry out studies of the extraction of chloridometalates. When L¹ was contacted with acidic zinc chloride

solutions a third phase formed which prevented further analysis. Consequently, the *tert*-butyl- substituted triamide (L^2) was synthesised from a precursor (2) that was prepared as shown in Scheme 2.

Scheme 2. Synthesis of the precursor for L^2 . Reagents & conditions: (i) ethanol, reflux, (ii) dichloromethane, $N_{2(g)}$, room temperature, (iii) dry acetone, $N_{2(g)}$, room temperature. $^{16, 17, 19-22, 25}$

As monoamido functionalised proligands having the structural sequence shown in Figure 1b were shown to have higher strength and selectivity than their di- and tri-functionalised analogues, the series of monoamido reagents was extended to include L^5 and L^6 . These were prepared from 3,5,5-trimethyl-hexanoyl chloride by conversion to the amide by reacting with aqueous ammonia followed by a one-pot Mannich reaction with formaldehyde and either di-n-hexylamine or di-2-ethylhexylamine to give L^6 or L^7 (Scheme 3).

$$\begin{array}{c|c}
CH_2O \\
NHR'
\end{array}$$

$$R'$$

Scheme 3. Preparation of the mono-amido reagents L^5 and L^6 ; $R = (CH_3)_3CCH_2CHCH_3CH_2$. Reagents and conditions: (i) $NH_{3(aq)}$, (ii) cooling and stirring overnight. $^{26, 33}$

The new reagents were characterised by NMR spectroscopy and mass spectrometry. Purity was determined from ¹H and ¹³C NMR spectra and confirmed by CHN analysis for the solid compounds. The structure of L¹ and L² was confirmed by X-ray crystallography (Figure 5). L²⁻⁶ showed sufficient solubility in toluene, both in neutral and protonated forms, to allow their performance as extractants to be compared with that of TEHA (Figure 3) which was taken as a model for the Alamine® reagents.

pH-Dependence of Zinc Loading: When pH-dependent M(II) loading experiments (see Experimental Section) were carried out, zinc uptake showed a marked dependence on the equilibrium pH (Figure 4), in accordance with a solvent extraction process as defined in Equation 5. The strengths of the extractants vary in the order $L^4 > L^5 > L^6 > L^3 > TEHA > L^2$. Despite confirming that the incorporation of an amide functionality into a trialkylamine structure such as TEHA enhances performance, the effect of increasing the number of amide moieties results in the inverse trend to that predicted: monoamide $(L^{4-6}) > diamide (L^3) > triamide (L^2)$, where L^2 was found to extract no zinc at all. Analysis of the organic phase using anion-exchange chromatography confirmed the preferential uptake of chloride for L^2 .

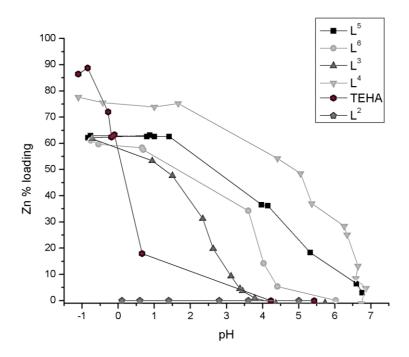


Figure 4. The pH dependence of chloridozincate loadings of 0.01 M toluene solutions of L^{2-6} upon contacting with an equal volume of an aqueous solution containing an excess of $ZnCl_2$ (0.01 M, total HCl/LiCl 6 M). 100% loading is based on the formation of $[(LH)_2ZnCl_4]$ as in Equation 5.

The crystal structures of L¹ and L² provide part of the explanation for this unexpected trend. The conformations of the proligands in the solid-state structures are strongly influenced by *intra*- and *inter*-molecular hydrogen bonding between amido units (see Figure 5). Dimers with very similar structures are formed by L¹ and L², with each molecule forming two *intra*- and one *inter*-molecular N-H---O=C hydrogen bonds. Such strong *intra*-molecular hydrogen bonding using the amido N-H units will reduce their availability for interactions with the chloridozincate. These issues are discussed more fully in the section dealing with DFT calculations.

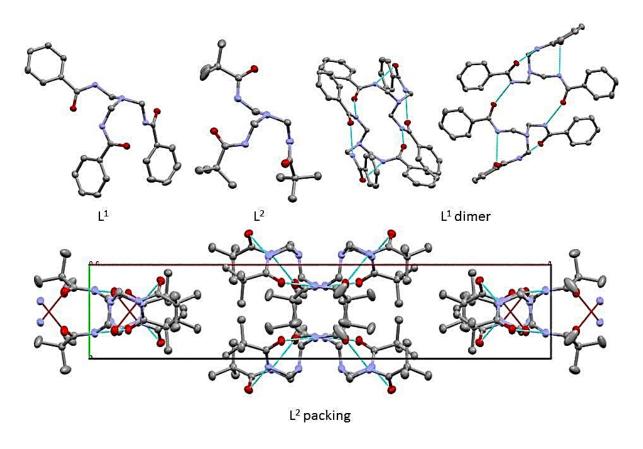


Figure 5. X-ray crystal structure of L^1 and L^2 showing a single molecule and the *intra*- and *inter*-molecular interactions in the solid state. Hydrogen atoms have been omitted for clarity.

The ability of the monoamido reagents (L^{4-6}) to load $ZnCl_4^{2-}$ efficiently from aqueous solutions with pH > 3 (see Figure 4) has important practical implications. It should be possible to recover zinc from solutions from which iron has been removed by precipitation on raising pH above 2.5, potentially providing a convenient route to separation and concentration of these metals from both secondary sources, such as galvanizing pickle liquors, $^{7,34-40}$ or from primary sources following oxidative chloride leaching of ores. 7,41,42 Efficient zinc uptake from 6 M chloride solutions implies selectivity for $ZnCl_4^{2-}$ loading over Cl_5^{1-} .

Whilst the pH dependence of zinc loading for L³-L6 is comparable to that previously reported for reagents having the amide/amine bond sequence b in Figure 1,43 it is clear that they behave differently in the context of maximum loadings. These fall in the range 60-75%, based on the formation of neutral 2:1 assemblies, [(LH)₂ZnCl₄], as in Equation 5. The lower maximum molar loadings than those for type b in Figure 1 do not arise from insufficient contact times being used as equilibrium is achieved with a five minute contact (see Figure 6).

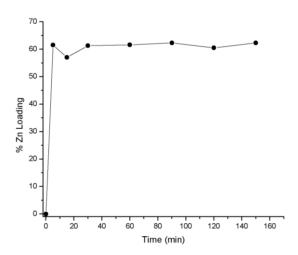


Figure 6. Time dependence of zinc loading by L⁴ under extractions conditions.

There is also no evidence to suggest that low purity or degradation of the reagents are responsible for loadings < 100%. A chloroform solution of L⁸, chosen because its truncated alkyl groups are likely to make it more hydrophilic than the reagents L¹⁻⁷, was stirred with 2 M HCl for three days, during which time, samples were removed, concentrated *in vacuo*, and analysed by ¹H NMR. Changes in chemical shifts are observed on protonation (see ESI), but thereafter no changes are observed which would be expected for the hydrolysis reaction shown in Figure 7.

Figure 7. Hydrolysis of L⁸.

In order to establish whether the stoichiometry of the extraction process is different from that shown in Equation 5, the dependence of zinc and chloride loading on L^4 concentration was investigated. The slope of a plot of logD $vs. \log[L^4]$, 2.12, is in reasonable agreement with the stoichiometry of extraction reaction in Equation 5.

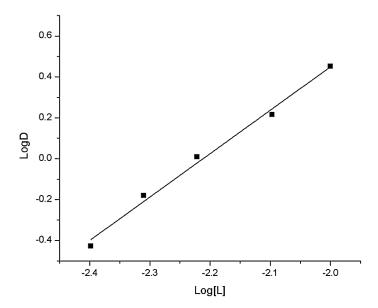


Figure 8. The best fit straight line $(log D_{Zn} = 2.12 log [L^4] + 4.69)$ relating zinc loading to concentration of extractant L^4 after contacting with a 0.003 M solution of ZnCl₂ in 6 M HCl.

The chloride content of the toluene extracts was determined by stripping into water. Over the range of extractant concentrations used in these experiments (0.004 to 0.01 mol/L, see Figure 9) c.a. 4.9 moles of chloride ion are present in the organic phase for each mole of zinc.

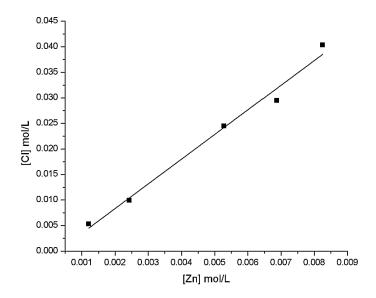


Figure 9. The relationship between the chloride concentration and zinc concentration in the toluene extracts for the extractions used for Figure 8, [Cl] = 4.82[Zn].

The maximum loading of zinc (as ZnCl₄²⁻ in [(L⁴H)₂ZnCl₄], Equation 5) is *ca*. 75% (see Figure 4). If the remaining 25% of L⁴ is fully protonated and forms the chloride salt [(L⁴H)Cl] in the organic phase then the calculated ratio of the concentrations of zinc to chloride in the organic phase will be 1:4.7 (see Experimental Section), which corresponds closely to that experimentally observed from Figure 9. Whilst the selectivity of L⁴ for ZnCl₄²⁻ over Cl⁻, as defined by the equilibrium constant for Equation 9, is high (e.g., 11x10⁵ for the extraction at highest acidity in Figure 4), the 6 M chloride concentration means that incomplete recovery results when the extractant L⁴ is not used in excess.

NMR experiments were used to confirm that these ligands operate *via* 'outer-sphere coordination' similar to reagents of Figure 1 a) and b). 11, 43 Comparison of the ¹H spectrum of the proligand, L⁴, with those of the complexes, [(L⁴H)₂ZnCl₄] and [(L⁴H)Cl] in deuterated toluene (Figure 10) provides evidence that complexation causes an increase in rigidity and significant shifts in the hydrogen bond donors' resonances representative of –NH and –CH groups which act as outer-sphere hydrogen bond donors. The splitting of resonance 'D' also indicates that the alkyl chains are no longer equivalent as –CH interactions restrain the ligand into a rigid conformation. The significant shift of the –NH resonances in the chloride complex indicate that the binding interactions at these positions are very strong would be expected with the chloride interaction.

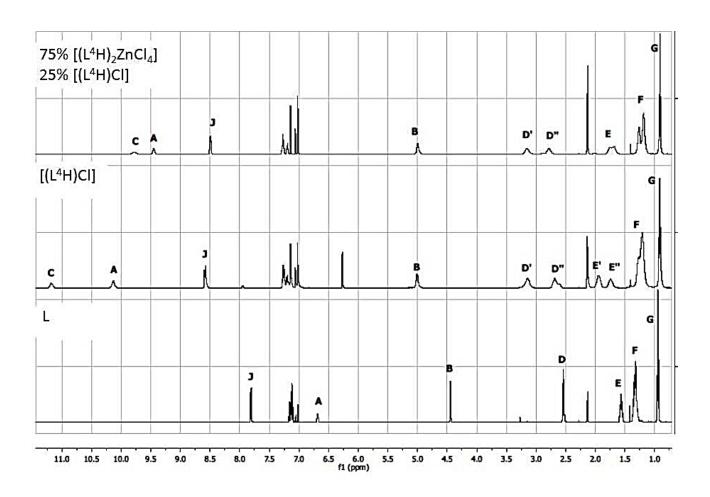


Figure 10. ¹H NMR spectra for [(L⁴H)Cl], L⁴ and [(L⁴H)₂ZnCl₄].

In order to probe further whether these systems form assemblies with unusual stoichiometries, which might also account for the Zn-loading values being lower than those predicted for the formation of 2:1 complex (Equation 5), a diffusion-ordered spectroscopy (DOSY) ¹H NMR study was carried out. This 2D NMR experiment, based on pulse-field gradient spin-echo NMR, allows comparison of diffusion rates which relate to properties such as size, shape, mass and charge of species in solution. ^{44, 45} TEHA was used as a standard, as it is known to form a 2:1 complex [(TEHAH)₂ZnCl₄]. ^{34, 46} If L⁴ forms a complex with an alternative stoichiometry its different size would be indicated by a different diffusion rate. There are only very small differences in the diffusion-induced separation in the resulting spectra (see ESI) suggesting that the complex formed by L⁴ is of a similar size to that of the TEHA complex, supporting the formulation of the former as [(L⁴H)₂ZnCl₄].

As mentioned above, the high strength of the monoamide reagents is such that zinc recovery could be achieved from an aqueous solution from which iron(III) has been removed by precipitation after raising pH. Data presented in Figure 11 show that it would also be possible to separate these metals by recovering the zinc selectively from an acidic solution containing iron(III) using L⁴, controlling the chloride concentration of the feed. A much higher chloride concentration (*ca.* 5 M) is required to achieve 50% recovery of iron than for zinc (*ca.* 1 M), and exclusive recovery of zinc from a mixed feed would be observed from a solution containing 2 M chloride. In contrast, the S-curves for Zn and Fe loading by TEHA lie much closer together and separation by solvent extraction is much less efficient.

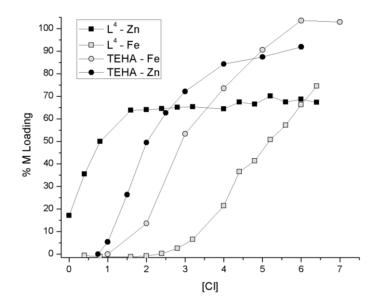


Figure 11. The dependence of loadings* of Fe(III) and Zn(II) by TEHA and L⁴ on chloride concentration. (* 100% loading is based on formation of [(LH)₂ZnCl₄] and [(LH)FeCl₄].

The high selectivity for ZnCl₄²⁻ over FeCl₄⁻ shown by L⁴ is remarkable as it defies the Hofmeister bias, which predicts that more highly charged anions are expected to be more difficult to extract into low polarity, water-immiscible solvents due to their higher hydration energies. ¹⁴ This striking feature is also shown ⁴³ by the related series of extractants (b in Figure 1) which form the six-membered proton chelate.

Hybrid-DFT Calculations: In attempting to understand the relative ease of formation of the neutral assemblies such as [(LH)₂ZnCl₄] in the extraction experiments, it is helpful to consider how the structures of the various reagents, particularly whether they contain one, two or three pendant amide groups, influence factors such as: (i) the ease of protonation of the proligands, L, to form the cationic species LH⁺, (ii) the arrangements of N-H and C-H hydrogen bond donors which can be presented to anions by the cationic extractants LH⁺, and (iii) the binding energies between the cationic extractants, LH⁺, and chloridometalate or chloride anions.

Proton Affinities of the Extractants: Hybrid-DFT calculations were used to evaluate the protonation affinities for the gas phase reaction shown in Equation 15. Providing the proton from a hydroxonium ion ensures that energies relate more closely to those in an extraction from an acidic aqueous solution. No provision was made for interactions between the cation LH⁺ and one or more water molecules. Variations in the nature of the *intra*- and *inter*-molecular hydrogen bonding motifs in the proligands, L, and their protonated forms are responsible for major differences in the ease of protonation of the mono-, di- and triamido reagents. The gas phase protonation of the monoamides is very favourable, because formation of the cation creates a

strong hydrogen bond between the ammonium NH group and the amido CO group without having to break any existing hydrogen bonds between amide units (compare the energy minimised forms of L⁴ and L⁴H⁺ in Figure 12). This contrasts markedly with the situation for the diamides which have a strong *intra*-molecular hydrogen bond in the neutral proligands, which has to be sacrificed to form a bifurcated hydrogen bond between the ammonium NH unit and the two carbonyl groups (compare L³ and L³H⁺ in Figure 12). As a consequence, the calculated proton affinity is less favourable for L³ than for L⁴ (-275 *vs.* -301 kJ mol⁻¹, see Table 1).

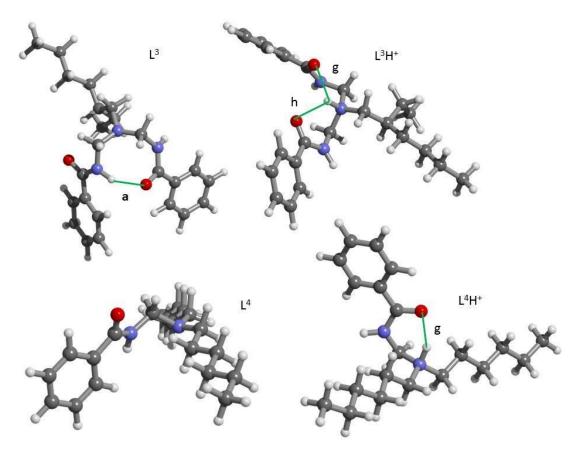


Figure 12. The energy-minimised structures of the proligands L^3 and L^4 and their protonated forms, L^3H^+ and L^4H^+ , calculated at B3LYP/6-31g(d,p). Significant *intra*-molecular hydrogen bonding interactions are marked.

Protonation of the triamides is less favourable than for the monoamides. Two energy-minimised structures were found for each of the proligands L¹ and L² (Figure 13). Those labelled as L¹ and L² were located starting from the atomic coordinates of the X-ray crystal structures, whereas L^{1*} and L^{2*} were found by altering the structure in Arguslab⁴⁷ to start from a different point on the potential energy surface. This was carried out a number of times in order to ensure the global minimum was obtained. The latter structures have *pseudo*-three-fold symmetry and form three *intra*-molecular amide bonds which collectively make up eight-membered rings

(Figure 13). As expected, these conformers are more stable than those with only two *intra*-molecular hydrogen bonds by around 41.7 kJ mol⁻¹ and 19.2 kJ mol⁻¹ for L¹ and L², respectively.

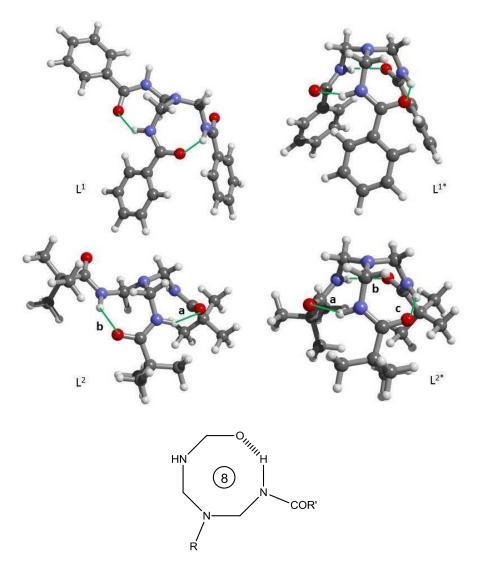


Figure 13. The energy-minimised structures located for the triamide proligands L^1 and L^2 showing the *intra*-molecular hydrogen bonds which define the 8-membered ring (inset).

The structures obtained upon protonation of L^1 and L^{1*} are shown in Figure 14. The resulting conformational changes for L^1 involve the loss of two amide-amide hydrogen bonds and the formation of the proton chelate unit (defined in Figure 1). In contrast, L^1H^{+*} retains the three *intra*-molecular hydrogen bonds observed in the proligand, but this prevents the ammonium N-H bond interacting with a carbonyl oxygen atom to form the proton chelate unit. Protonation of the amine group in L^{1*} causes the nitrogen atom to be displaced from the plane defined by the three carbon atoms of the methylene groups in the capping unit (Figure 14). Similar behaviour is observed for L^2 and L^{2*} (Figure 14), with the conformer containing the proton chelate unit being the more stable.

The difference in energy between the *lowest energy* forms of the proligand (L) and cationic ligand (LH⁺) was used to calculate the proton affinities shown in Table 1. The value for L^2 (-266 kJ mol⁻¹) is less favourable than those for the di- and monoamides, L^3 and L^4 . The decrease in proton affinity with the number of amide groups present in the reagent (monoamides > diamides > triamides) appears to be largely a consequence of protonation being accompanied by loss of *intra*-molecular hydrogen bonding between amide groups. The formation of neutral complexes $[(LH)_nMCl_4]$ as in Equations 12 and 14 is favourable and the observed order of strength as zinc extractants (monoamide L^4 > diamide L^3 > triamide L^2) follows the order of their proton affinities. The binding enthalpy of the ligands is also an important criterion in contributing towards the overall formation enthalpy of the complex. A favourable binding enthalpy could compensate for an unfavourable proton affinity. These binding enthalpies will depend on the nature and disposition of hydrogen bond donors in the cationic ligands and how they interact with the outer-coordination spheres of the chloridometalate and will contribute to both the strength and selectivity of the ligands as anion extractants.

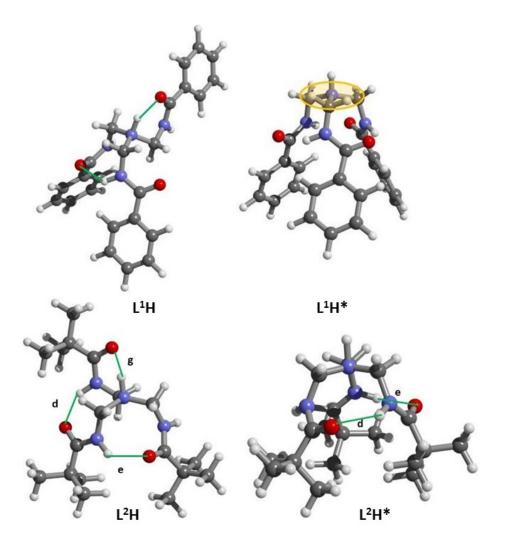


Figure 14. The energy-minimised structures of the two possible confirmations of L^1H^+ and $L2H^+$. The orange disc indicates the distorted 'C-C-C' plane of L^1H^{+*} . For L^2H^{+*} , bond 'f' (C=O---HN) is obstructed from sight.

The strength of the NH---O bonding interactions in the proligands (L) and ligands (LH $^+$) may be compared using the natural bond order (NBO)-derived stabilisation energies and the calculated interatomic distances, the most significant of which are listed in Table 1. In the cationic ligands (LH $^+$), the ammonium N-H to carbonyl bonding interaction is significantly stronger than any amido N-H to carbonyl interaction. This most likely arises because the geometry is more favourable for the bonding contact in the six-membered proton chelate unit in the former than in the eight-membered ring in the latter. The shortest and strongest hydrogen bond is observed in the protonated form of L 4 , which is also the strongest zinc extractant on the basis of the experimental data reported above.

		Extractant								
Bonding contacts (a-h) in		L^{2a}		L^{2*a}		L^3		L^4		
Figures 12, 13 and 14		r	E	r	E	R	E	r	E	
NH _{amide} O=C	a	2.00	44.5	2.12	25.8	1.96	44.9	-	-	
in L	b	2.03	21.4	2.12	25.9	-	-	-	-	
	c	-	-	2.12	25.6	-	-	-	-	
NH _{amide} O=C	d	2.10	24.9	2.12	26.7	-	-	-	-	
in LH ⁺	e	2.08	17.0	2.12	26.3	-	-	-	-	
	f	-	-	2.12	26.4	-	-	-	-	
NH _{ammonium} O=C	g	1.85	72.5	-	-	2.11	28.9	1.8	79.5	
in LH ⁺	h	-	-	-	-	2.13	27.3	-	-	
Calculated Enthalpies (kJ mol ⁻¹)										
		L^2	2			L^3		L^4	L^4	
PA		-265.9				-274.5		-301.5	-301.5	
BE in [(LH)Cl]	-406.8				-398.7		-378.8			
BE in [(LH) ₂ ZnCl ₄]	-12687.1				-12643.8		-12670.2			
BE in [(LH)FeCl ₄]	-				-		-244.8			
FE of [(LH) ₂ ZnCl ₄]		-13218.8				-13192.9		-1327	-13273.1	
FE of [(LH)Cl]		-672.7				-673.2		-680.2		
FE of [(LH)FeCl ₄]		-				-		-546.3	-546.3	
ZnCl ₄ ² -/Cl ⁻ exchange ^b		-11844.8				-11848.9		-1190	-11905.3	

Table 1. Calculated lengths (r/Å) and strengths ($E/kJmol^{-1}$) of the interatomic hydrogen bonding contact distances for the NH---O=C interactions in the neutral and protonated forms of L²-L⁴, together with the proton affinities (PA) of the extractants, the binding enthalpies (BE) of LH⁺ to anions in the [(LH)Cl] and [(LH)₂ZnCl₄] complexes and the formation enthalpies (FE) of the [(LH)₂ZnCl₄], [(L⁴H)Cl] and [(L⁴H)FeCl₄] complexes. ^aFigures showing the energy-minimised structures of L₂H⁺ and L₂H⁺* are provided in supplementary information. ^bEnthalpy for the anion exchange reaction 2[(LH)Cl] + ZnCl₄²- \rightleftharpoons [(LH)₂ZnCl₄] + 2Cl⁻¹ (kJ mol⁻¹).

The binding enthalpies of L²H⁺, L³H⁺ and L⁴H⁺ to ZnCl₄²⁻, which correspond to the energy released when two moles of the pre-formed cationic ligand and one mole of chloridozincate anion are brought together (Equation 17), are shown in Table 1. The stronger binding of L²H⁺ than L³H⁺ and L⁴H⁺ to the outer sphere of ZnCl₄²⁻ may result from L²H⁺ presenting two amido hydrogen bond donors to the metalate anion. The strongest of the interactions are shown in Figure 15 and in Table 2. Some of these NH---Cl and CH---Cl interactions are accompanied by weaker interactions with other coordinated chlorine atoms, leading to very unsymmetrical bifurcated "hydrogen bonds". The more favourable NH---Cl interactions are often complemented by those from C-H groups. The four strongest CH---Cl interactions formed by L²H⁺ are labelled (e)-(i) in Figure 15 and have energies that are approximately half those of the N-H---Cl bonding interactions. A common feature of the chloridozincate complexes formed by L²H⁺, L³H⁺ and L⁴H⁺ is that there are no bonding interactions to the outer sphere made by their ammonium N-H groups. In all cases, these interact instead with an amido oxygen atom to form the proton chelates which are a characteristic of these ligands.

Bonding contacts (a-o) in Figure		$[(L^2H)_2ZnCl_4]$		$[(L^3H)_2ZnCl_4]$		$[(L^4H)_2ZnCl_4]$	
15		r	E	r	E	r	E
N-H _{amide} Cl	a	2.45	31.8	2.31	52.8	2.21	74.8
	b	2.58	17.7	2.50	21.5	2.15	85.7
	c	2.53	21.5	2.38	39.7	-	-
	d	2.44	31.7	-	-	-	-
C-HCl	e	2.64	8.1	2.34	38.5	2.62	9.1
	f	2.73	11.4	2.83	5.3	2.87	5.8
	g	2.74	17.3	2.67	14.9	2.44	28.0
	h	2.67	14.2	2.71	10.0	2.83	4.8
	i	-	-	-	-	2.84	4.5
N-H _{amide} O=C	j	1.97	38.1	-	-	-	-
	k	1.94	36.9	-	-	-	-
N-H _{ammonium} O=C	1	1.91	50.5	2.39	3.7	1.99	44.5
	m	1.92	49.3	2.16	23.2	1.89	63.9
	n	-	-	2.56	2.9	-	-
	0	-	-	1.98	49.5	-	-

Table 2. Calculated lengths (r/Å) and strengths $(E/kJmol^{-1})$ of the N-H---O and N-H---Cl interactions in $[(L^2H)_2ZnCl_4]$, $[(L^3H)_2ZnCl_4]$ and $[(L^4H)_2ZnCl_4]$. For the NH---Cl interactions, only those with bonding energies > 10% of the strongest are listed, and for CH---Cl interactions, only those with bonding energies > 5% of the strongest NH---Cl interaction are included.

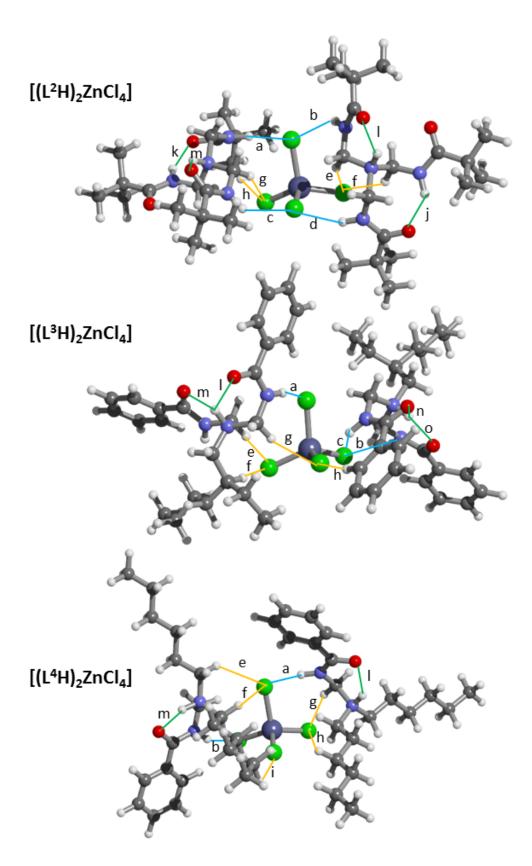


Figure 15. The energy-minimised structures of $[(L^2H)_2ZnCl_4]$, $[(L^3H)_2ZnCl_4]$ and $[(L^4H)_2ZnCl_4]$ showing the strongest NH---Cl and CH---Cl interactions (in blue and orange, respectively) and the *intra*-ligand hydrogen bonds formed by the "chelated proton" (in green).

As might be expected, the strongest bonding interactions in the outer sphere of $ZnCl_4^{2-}$ are those involving N-H_{amide}---Cl contacts, which average 47 kJ mol⁻¹. In complexes where it is not conformationally possible for all the amido N-H groups to be directed towards a single chloridozincate ion (as with L^2H^+), or where there is only one amido group in the ligand (as in L^4H^+) the strong interactions are complemented by an array of weaker CH---Cl interactions (see Figure 15), which average 13 kJ mol⁻¹. The formation of a large number of weakly bonding interactions from N-H and C-H groups appears to be preferred by the charge-diffuse ("soft") chloridozincate anion. The "harder" chloride ion shows a strong preference for N-H donors (see below).

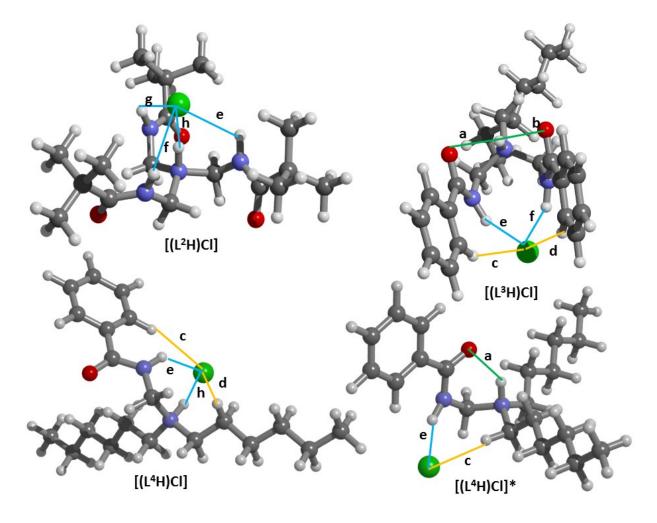


Figure 16. The energy-minimised structures of [(L²H)Cl], [(L³H)Cl] and of two conformers of [(L⁴H)Cl] and showing NH---Cl interactions (in blue), CH---Cl interactions (in orange) and the *intra*-ligand hydrogen bonds (in green).

The relative values of the binding enthalpies of an LH⁺ ligand to Cl⁻, ZnCl₄²⁻ or FeCl₄⁻ will contribute to its selectivity as a solvent extractant in the experiments described above. The calculated gas phase values of these binding enthalpies (Table 1) for the protonated form of the most effective zinc extractant, L⁴H⁺, become more

favourable in the order $FeCl_4^- < Cl^- << ZnCl_4^{2-}$, which is consistent with the selectivity of extraction of these anions observed in the solution experiments. The greater binding energy of a single molecule of L^4H^+ to $ZnCl_4^{2-}$ than to $FeCl_4^-$ (-6335 *c.f.* -245 kJ mol⁻¹), presumably arises from the higher negative charge on $ZnCl_4^{2-}$ and is reflected by the considerably stronger NH---Cl interactions (an average of 80 kJ mol⁻¹ in the $ZnCl_4^{2-}$ complex compared to 25 kJ mol⁻¹ in the $FeCl_4^-$ complex) and CH---Cl interactions which are a maximum of 28 kJ mol⁻¹ compared to 8 kJ mol⁻¹ in the $ZnCl_4^{2-}$ and $FeCl_4^-$ complexes (Tables 2 and 3; data for $FeCl_4^-$ binding is contained in the supplementary information).

Bonding contacts (a-h) in Figure 16		$[(L^2H)Cl]$		[(L³H)Cl]		[(L ⁴ H)Cl]		[(L ⁴ H)Cl]*	
		r	E	r	E	r	E	r	E
N-H _{ammonium} O=C	a	-	-	2.22	17.5	-	-	1.87	71.0
	b	-	-	2.31	9.9	-	-	-	-
C-HCl	c	-	-	2.82	4.9	2.88	7.1	2.52	26.6
	d	-	-	2.96	5.1	2.85	4.6	-	-
N-H _{amide} Cl	e	2.81	6.4	2.09	118.9	2.38	39.3	1.96	204.4
	f	2.81	5.5	2.12	111.5	-	-	-	-
	g	2.82	4.8	-	-	-	-	-	-
N-H _{ammonium} Cl	h	1.88	310.3	-	-	1.88	422.2	-	-

Table 3: Calculated lengths (r) in Å and strengths (*E*) in kJ mol⁻¹ of NH---O, NH---Cl and NH---Cl interactions in $[(L^2H)Cl]$, $[L^3H)Cl]$, $[(L^4H)Cl]$. For NH---Cl interactions only those > 10% of the strongest are listed and for CH---Cl interactions only those > 5% of the strongest NH---Cl interaction are included. There are no significant NH_{amide}---O=C or CH---O=C interactions.

The binding enthalpy of the ligands to chloride becomes more favourable in the order $L^4H^+ < L^3H^+ < L^2H^+$. L^2H^+ provides a particularly favourable binding site for a chloride ion (Figure 16) in which the ammonium and all three amido N-H groups are directed towards the anion. Of the two lowest energy conformations of [(L^4H)Cl] shown in Figure 16, that on the left with both the amido and ammonium N-H groups directed at the chloride ion is more favourable by 29 kJ mol⁻¹ than that on the right which uses only the amido N-H to interact with the chloride and has the ammonium N-H weakly chelated by the carbonyl oxygen atom. The data in Table 3 show that the N-H groups form much stronger bonding interactions with Cl⁻ than with Z^{-1} (Table 2). This presumably arises from the higher charge:radius ratio on the former. The strongest hydrogen bonds to chloride are provided by the cationic ammonium N-H units, *e.g.*, contacts 'h' in structures [(L^2H)Cl] and [(L^4H)Cl] in Figure 16 with calculated strengths of 311 and 422 kJ mol⁻¹, respectively. An NBO analysis of the chloride complexes of L^4 in Figure 16 (with values in Table 3) also suggests that the ammonium N-H----Cl interactions are much stronger than the most favourable C-H---Cl interactions, *e.g.*, 422 compared to 7 kJ mol⁻¹ (for 'h' and 'c' in structure [(L^4H)Cl]*, respectively). This can be ascribed to a much greater

electrostatic contribution to the bonding being associated with the chloride anion and cationic ammonium nitrogen atom. In the alternative conformer [(L⁴H)Cl]*, there is a strong hydrogen bonding interaction (71 kJ mol⁻¹) for interaction 'a' in the proton chelate ring. The strongest CH---Cl interaction for conformer [(L⁴H)Cl]*, is 'c' (27 kJ mol⁻¹) and the dominant interaction is the amido NH---Cl contact ['e', 204 kJ mol⁻¹].

Calculated enthalpies of formation of the [(LH)_nMCl₄] assemblies: The gas phase formation enthalpies of the [(LH)₂ZnCl₄] complexes (labelled FE in Table 1) indicate that the ease of formation follows the order L⁴> L²> L³. This differs from the order observed in solvent extraction experiments (L⁴> L³>> L²) but can be rationalised by taking into account the fact that the effective strength of a solvent extractant depends on the selectivity of the reagents for chloridometalate over chloride, *i.e.*, on the position of the equilibrium: $2[(LH)Cl] + ZnCl_4^{2-} \Rightarrow [(LH)_2ZnCl_4] + 2Cl^{-1}$. The L²H⁺ cation forms a particularly stable chloride complex, [(L²H)Cl, see above], and consequently has the worst selectivity for chloridozincate over chloride (see Table 1). This results in no significant zinc uptake under the conditions used for solvent extraction in which the maximum concentration of $ZnCl_4^{2-}$ is 0.01 M compared to 6.0 M [Cl⁻].

The superior performance of the monoamide reagent L⁴ arises from it having the most favourable proton affinity (PA in Table 1), and whilst L⁴H⁺ does not have as favourable binding enthalpy to ZnCl₄²⁻ as L²H⁺ (BE in Table 1), the latter has a very strong preference to bind chloride ions which accounts for it showing no zinc loading in practice.

Conclusions

The new amido-amine reagents should allow more effective recovery of zinc from acidic chloride streams than conventional trialkylamines, and in some cases they show remarkably high selectivity for zinc over iron, a separation which is necessary for processing most pregnant chloride leach solutions. Whilst the introduction of amido groups into the reagents clearly enhances their properties over "simple" amines, it needs to be understood that the presence of more than one amide unit can have detrimental effects in: (i) facilitating amide:amide hydrogen bonding which can reduce the solubility in the non-polar solvents used in solvent extraction processes, (ii) enhancing binding strengths to chloride ions and thus reducing the selectivity for extraction of ZnCl₄²⁻ over Cl⁻ and (iii) lowering the proton affinity of the reagents because protonation results in the breaking of *intra*-molecular amide-amide hydrogen bonds.

DFT calculations have proved to be very useful in understanding the structure activity relationships of this new class of reagent.

Notes and references

[#]Footnote: Earlier work^{15, 48, 49} with the other amido/amine "proton chelating" reagents (a and b in Figure 1) provides no evidence for formation of hydrated forms of the extracted assemblies, [(LH)_nMCl₄], in marked contrast with extraction processes involving recovery of metalates from acidic solutions using phosphine oxides and related reagents.^{50, 51}

- [1] Stensholt, E. O.; Zachariasen, H.; Lund, J. H., Miner. Proc. Extr. Metall. 1986, 95, C10-C16.
- [2] Stensholt, E. O.; Dotterud, O. M.; Henriksen, E. E.; Ramsdal, P. O.; Stalesen, F.; Thune, E., *CIM Bull.* **2001**, *94*, 101.
- [3] Dutrizac, J. E., Hydrometallurgy 1992, 29, 1-45.
- [4] Gangazhe, T. In *Zinc extraction from high chloride liquors*, 19th International Solvent Extraction Conference, Santiago, Chile, 2011; Valenzuela L., F.; Moyer, B. A., Eds.
- [5] Tozawa, K.; Nishimura, T.; Akahori, M.; Malaga, M. A., *Hydrometallurgy* **1992**, *30*, 445-461.
- [6] Gnoinski, J.; Sole, K. C. In *The influence and benefits of an upstream solvent extraction circuit on the electrowinning of zinc sulfate media. The Skorpion zinc process.*, Hydrometallurgy. Proceedings of the sixth International Symposium, 2008; Young, C. A.; Taylor, P. R.; Anderson, C. G.; Choi, Y., Eds. Society for mining, metallurgy an exploration, Inc.
- [7] Cole, P. M.; Sole, K. C., J. S. Afr. Inst. Min. Metall. 2002, 102, 451-456.
- [8] McDonald, R. G.; Whittington, B. I., Hydrometallurgy 2008, 91, 56-69.
- [9] Flett, D. S. In *Chloride Hydrometallurgy for Complex Sulphides: a Review*, Chloride Metallurgy, 32nd Annual Hydrometallurgy Meeting, 2002; Peek, E.; Van Weert, G., Eds. 2002; p 255.
- [10] 1Winand, R., Hydrometallurgy 1991, 27, 285-316.
- [11] 1Ellis, R. J.; Chartres, J.; Henderson, D. K.; Cabot, R.; Richardson, P. R.; White, F. J.; Schroder, M.; Turkington, J. R.; Tasker, P. A.; Sole, K. C., *Chemistry: A European Journal* **2012**, *18*, 7715-28.
- [12] http://www.meab-mx.se Metallextraktion AB webpage. (24/04/12),
- [13] Hofmeister, F., Archiv. Exptl. Pathol. Pharmakol. 1888, 24.
- [14] Moyer, B. A.; Bonnesen, P. V.; Custelcean, R.; Delmau, L. H.; Hay, B. P., Kem. Ind. 2005, 54, 65-87.

- [15] Ellis, R. J.; Chartres, J.; Sole, K. C.; Simmance, T. G.; Tong, C. C.; White, F. J.; Schroder, M.; Tasker, P. A., Chem. Commun. 2009, 583-585.
- [16] Csomos, P.; Fodor, L.; Bernath, G.; Csampai, A.; Sohar, P., Tetrahedron 2008, 64, 8646-8651.
- [17] Csomos, P.; Fodor, L.; Bernath, G.; Csampai, A.; Sohar, P., Tetrahedron 2009, 65, 1475-1480.
- [18] Moe, G. R.; Sayre, L. M.; Portoghese, P. S., Tetrahedron Lett. 1981, 22, 537-540.
- [19] Basha, A.; Weinreb, S. M., Tetrahedron Lett. 1977, 1465-1468.
- [20] Albericio, F.; Grandas, A.; Porta, A.; Pedroso, E.; Giralt, E., Synthesis 1987, 271-272.
- [21] Weaver, J. W.; Schuyten, H. A.; Frick, J. G.; Reid, J. D., J. Org. Chem. 1951, 16, 1111-1116.
- [22] Kiso, Y.; Yoshida, M.; Kimura, T.; Fujiwara, Y.; Shimokura, M., Tetrahedron Lett. 1989, 30, 1979-1982.
- [23] Popovski, E.; Bogdanov, J.; Najdoski, M.; Hey-Hawkins, E., *Molecules* **2006**, *11*, 279-285.
- [24] Popovski, E.; Klisarova, L.; Vikic-Topic, D., *Molecules* **2000**, *5*, 927-936.
- [25] Popovski, E.; Klisarova, L.; Vikic-Topic, D., Synthetic Communications 1999, 29, 3451-3458.
- [26] Dowbenko, R.; Salem, A. N.; Christensen, R. M., J. Org. Chem. 1963, 28, 3458-3460.
- [27] Fritz, J. S.; Gjerde, D. T., Ion Chromatography. Wiley-VCH: 2000.
- [28] Frisch, M. J.; Trucks, G. W.; Schlegel, H. B.; Scuseria, G. E.; Robb, M. A.; Cheeseman, J. R.; Scalmani, G.; Barone, V.; Mennucci, B.; Petersson, G. A.; Nakatsuji, H.; Caricato, M.; Li, X.; Hratchian, H. P.; Izmaylov, A. F.; Bloino, J.; Zheng, G.; Sonnenberg, J. L.; Hada, M.; Ehara, M.; Toyota, K.; Fukuda, R.; Hasegawa, J.; Ishida, M.; Nakajima, T.; Honda, Y.; Kitao, O.; Nakai, H.; Vreven, T.; Montgomery, J., J. A.; Peralta, J. E.; Ogliaro, F.; Bearpark, M.; Heyd, J. J.; Brothers, E.; Kudin, K. N.; Staroverov, V. N.; Kobayashi, R.; Normand, J.; Raghavachari, K.; Rendell, A.; Burant, J. C.; Iyengar, S. S.; Tomasi, J.; Cossi, M.; Rega, N.; Millam, N. J.; Klene, M.; Knox, J. E.; Cross, J. B.; Bakken, V.; Adamo, C.; Jaramillo, J.; Gomperts, R.; Stratmann, R. E.; Yazyev, O.; Austin, A. J.; Cammi, R.; Pomelli, C.; Ochterski, J. W.; Martin, R. L.; Morokuma, K.; Zakrzewski, V. G.; Voth, G. A.; Salvador, P.; Dannenberg, J. J.; Dapprich, S.; Daniels, A. D.; Farkas, Ö.; Foresman, J. B.; Ortiz, J. V.; Cioslowski, J.; Fox, D. J. *Gaussian 09, Revision A.1*, Wallingford CT, 2009.
- [29] Becke, A. D., J. Chem. Phys. 1993, 98, 1372-1377.
- [30] Chandra, A. K.; Goursot, A., J. Phys. Chem. 1996, 100, 11596-11599.

- [31] Boys, S. F.; Bernardi, F., Mol. Phys. 1970, 19.
- [32] Glendening, E. D.; Reed, A. E.; Carpenter, J. E.; Weinhold, F. NBO 3.0 Program Manual.
- [33] Singh, G. B.; Bindal, M. C.; Dixit, S. C., J. Indian Chem. Soc. 1975, 52, 438-439.
- [34] Regel, M.; Sastre, A. M.; Szymanowski, J., Environ. Sci. Technol. 2001, 35, 630-635.
- [35] Cierpiszewski, R.; Miesiac, I.; Regel-Rosocka, M.; Sastre, A. M.; Szymanowski, J., *Ind. Eng. Chem. Res.* **2002**, *41*, 598-603.
- [36] de Morais, C. A.; Carvalho, D. H.; F., R. S. D.; Mansur, M. B. In *Separation of zinc from iron(II) in spent pickling effluents produced by the hot-dip galvanizing industry by liquid-liquid extraction*, 18th International Solvent Extraction Conference, Tuscon, USA, 2008; Moyer, B. A., Ed.
- [37] Lum, K. H.; Kentish, S. E.; Stevens, G. W. In *Recovery of zinc from hot-dip galvanising effluent using tri-n-butyl phosphate*, 19th International Solvent Extraction Conference, Santiago, Chile, 2011; Valenzuela L., F.; Moyer, B. A., Eds.
- [38] Regel-Rosocka, M., J. Hazard. Mater. 2010, 177 57-69.
- [39] Regel-Rosocka, M.; Wisniewski, M., Hydrometallurgy 2011, 110, 85-90.
- [40] Niemczewska, J.; Cierpiszewski, R.; Szymanowski, J., Desalination 2004, 162, 169-177.
- [41] Baba, A. A.; Adekola, F. A., *Hydrometallurgy* **2011**, *109*, 187-193.
- [42] Kariuki, S.; Moore, C.; McDonald, A. M., Hydrometallurgy 2009, 96, 72-76.
- [43] Ellis, R.; J. Chartres; Tasker, P. A.; Sole, K. C., Solvent Extr. Ion Exch. 2011, 29, 657-672.
- [44] Huo, R.; Wehrens, R.; van Duynhoven, J.; Buydens, L. M. C., Anal. Chim. Acta 2003, 490, 231-251.
- [45] Brand, T.; Cabrita, E. J.; Berger, S., Modern Magnetic Resonance 2008, 135–143.
- [46] Jha, M. K.; Kumar, V.; Singh, R. J., Solvent Extr. Ion Exch. 2002, 20, 389-405.
- [47] Thompson, M. A. ArgusLab 4.0.1. Planaria Software LLC. http://www.arguslab.com, Seattle, WA.
- [48] Bell, K. J.; Westra, A. N.; Warr, R. J.; Chartres, J.; Ellis, R.; Tong, C. C.; Blake, A. J.; Tasker, P. A.; Schroder, M., *Angew. Chem. Int. Ed.* **2008**, *47*, 1745-1748.
- [49] Warr, R. J.; Westra, A. N.; Bell, K. J.; Chartres, J.; Ellis, R.; Tong, C.; Simmance, T. G.; Gadzhieva, A.; Blake, A. J.; Tasker, P. A.; Schroder, M., *Chemistry-A European Journal* **2009**, *15*, 4836-4850.

- [50] Ribeiro, L. C.; Paiva, A. P. In N,N-disubstituted monoamides in the recovery of iron(III) from chloride media, 19th International Solvent Extraction Conference, Santiago, Chile, 2011; Valenzuela L., F.; Moyer, B. A., Eds.
- [51] Isaac Yu Fleitlikh; Gennady L. Pashkov; Natalia A. Grigorieva; Lidia K. Nikiforova; Logutenko, O. A. In *Zinc extraction from sulphate media with systems based on Cyanex 301*, 19th International Solvent Extraction Conference, Santiago, Chile, 2011; Valenzuela L., F.; Moyer, B. A., Eds.