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## **Ti<sub>2</sub>AlC and Ti<sub>3</sub>SiC<sub>2</sub> MAX Phase Foams: Processing, Porosity Characterization and Connection between Processing Parameters and Porosity**

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### **ABSTRACT**

MAX phases Ti<sub>2</sub>AlC and Ti<sub>3</sub>SiC<sub>2</sub> foams with controlled porosity and pore size were produced using the space holder method. The foams were processed using water-leachable crystalline carbohydrate as space holder that involves: mixing, cold isostatic pressing, dissolution and sintering. Three combinations of volume percentage (20%-60%) and size distribution (250-1000 µm) of space holder were introduced during mixing. The foams were characterized and compared with the material without space holder. The characterization included: morphology (overall, open and closed porosity by Archimedes method) and gas permeability. Foams with porosity up to about 60 vol% and pore size distribution ranging from about 250 to 1000 µm were produced. Experimental porosity was compared to the theoretical expected porosity. The results show a bimodal porosity that can be customized by the sintering and the space holder. This study connects the processing parameters to the porosity created and allows control of porosity and pore size to produce tailor-made properties.

Keywords: MAX phases, Ti<sub>2</sub>AlC, Ti<sub>3</sub>SiC<sub>2</sub>, porous materials, eco-friendly processing, water-soluble space holder, permeability.

### **1. INTRODUCTION**

MAX phases were first discovered in the 1967 by Jeitschko and Hans Nowotny [1, 2] but they were not studied in depth until the 90's by Barsoum [3]. The MAX phases are a new family of materials with remarkable properties which make them interesting for industry because they combine the properties of both metals and ceramics. MAX phases are ternary compounds generally denominated by the letters "M", "A", and "X" where: M is an early transition metal, A is an A-group element and X is carbon or nitrogen [4, 5]. They are combined stoichiometrically by the formula: M<sub>n+1</sub>AX<sub>n</sub> where "n" is a number between 1 and 3. At the moment there are more than 60 MAX phases discovered. This study is focused on the Ti<sub>2</sub>AlC and Ti<sub>3</sub>SiC<sub>2</sub> MAX phases available commercially.

At the moment most of the research on Ti<sub>2</sub>AlC and Ti<sub>3</sub>SiC<sub>2</sub> MAX phases is focused in the solid material and there are few studies on porous material [6-22]. Porous MAX phases offer a better combination of properties than the conventional porous ceramics since they achieve good mechanical properties at high temperature in addition to being electrically and thermally conductive and also having excellent machinability. Porous MAX phases can find applications in: substrates for catalysts devices, porous electrodes, chemical filters, electrolyte clapboards, hot gas filtration, etc [23, 24]. Research in processing of porous materials is focused on flexibility in control of porosity from processing parameters that allows tuning the porosity to tailor-make the final foam properties.

This study is focused on controlling the porosity of the foams adjusting the processing parameters. The processing method employed is the space holder method in which the porosity is introduced by the space holder and controlled by modification of the space holder size and the powder/space holder ratio. The variation of porosity with the addition of space holder was studied in terms of open, closed and overall porosity and adjusted to a linear equation. The effect of pore size and amount of porosity on gas permeability was studied for both materials.

## 2. EXPERIMENTAL

Two commercial powders were employed:  $Ti_2AlC$  and  $Ti_3SiC_2$  MAX phases from Sandvik (Sweden). Both were characterized. The average particle size was measured by Mastersizer 2000 equipment:  $D_{50}=9.801 \mu m$  for  $Ti_2AlC$  and  $D_{50}=5.582 \mu m$  for  $Ti_3SiC_2$ . The specific surface area was measured by using BET:  $2.7674 m^2/g$  ( $Ti_2AlC$ ) and  $2.3670 m^2/g$  ( $Ti_3SiC_2$ ). The density was determined using an Accupyc helium pycnometer:  $4.122 g/cm^3$  ( $Ti_2AlC$ ) and  $4.6970$  for  $Ti_3SiC_2$ . After the powder characterization, the powders were mixed with 2% of lubricant (Acrowax C:  $C_{38}H_{76}N_2O_2$ , Lonza) to facilitate the compaction. The space holder was sieved into three size distributions: 250–400  $\mu m$ , 400–800  $\mu m$ , and 800–1000  $\mu m$ . Then, three powder/space holder ratios in vol.% were mixed for each space holder size distribution resulting in nine different mixtures. Next, the mixtures were introduced inside a silicone mold and sealed. They were compacted by the cold uniaxial pressing (CIP) and pressed during 10 minutes at 400 MPa. The green bodies were soaked in distilled water under controlled conditions. Four conditions were studied in order to optimize the dissolution of the space holder. Then they were dried under controlled conditions: 30 °C during 24h. The samples were sintered in a vacuum furnace at  $10^{-5}$  mbar. The thermal cycle included a 30 min plateau at 400 °C for delubrication purposes, and then they were sintered during 4 h at 1400 °C ( $Ti_2AlC$ ) and at 1350 °C ( $Ti_3SiC_2$ ). The samples were mechanized in a cylindrical shape with a lathe to obtain uniform geometry: constant diameter along the axe and plane-parallel bases. The porosity was calculated by Archimedes' method following the ASTM C20-00 standard and using ethanol to infiltrate the samples and as immersion medium. The samples were metallographically prepared: they were cut, inlaid in resin, grinded with SiC sandpaper and polished with diamond from 3  $\mu m$  to 0.1  $\mu m$ . Then, the samples' microstructure was observed by scanning electron microscope (SEM; Philips XL-30).

The gas permeability in the radial direction for each foam condition was determined using a special measuring cell. This equipment measures the permeability by emission of a flow of nitrogen gas through the probe. The pressure in the sample increases and is monitored. Each sample was drilled leaving a central hole (2mm in diameter). The gas permeability was calculated as the mass flow (Q) from the integration of the Forchheimer equation [25].

## 3. RESULTS AND DISCUSSIONS

Space holder elimination was monitored by measuring mass after the dissolution process in order to ensure complete space holder removal. The mass of the sample before and after dissolution was compared to the space holder mass content in the sample prior to dissolution, so a mass loss of 100% corresponds to complete removal of the space holder. Different dissolution conditions of temperature, time and stirring were compared (table 1). Condition 1, was studied only for  $Ti_2AlC$ , for which 71 % mass loss was achieved. Then, the temperature and time were raised, in condition 2, resulting in an elimination of 85% for  $Ti_3SiC_2$  and an increase of 2% of mass loss for  $Ti_2AlC$ . Next, the time was increased up to 48h, in condition 3, and the mass loss achieved was: 96% for  $Ti_3SiC_2$  and 85% for  $Ti_2AlC$ . Finally, stirring was added, in condition 4; and no significant variations were found for  $Ti_3SiC_2$  and for  $Ti_2AlC$  100% of mass loss was achieved. For  $Ti_3SiC_2$  higher mass loss than  $Ti_2AlC$  was achieved under the same conditions without stirring.

Table 1. Details of dissolution conditions employed: time, temperature and stir.

Leaching condition	Time (h)	Temperature (°C)	Stir
1	12	60	No
2	24	70	No
3	48	70	No
4	48	70	Yes

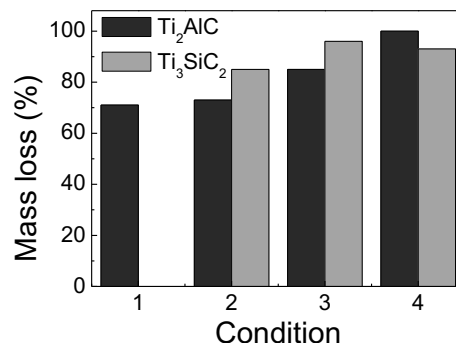


Figure 1. Variation of mass loss (%) of space holder after soaking under different dissolution conditions for  $Ti_2AlC$  and  $Ti_3SiC_2$ .

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Figure 2 shows the results, for both materials, of porosity for the three amounts of space holder introduced in the mixture. The porosity was studied in terms of: open, closed and overall porosity.  $Ti_2AlC$  shows that porosity is mainly closed up to 40 vol.% of space holder and from 40 vol.% up to 60 vol.% of space holder, porosity is mostly open, for all space holder sizes.  $Ti_3SiC_2$  exhibits mainly open porosity for all amounts of space holder and for all space holder size distributions. Porosity, for both materials, increases with the addition of space holder, and the addition of space holder increases open porosity. Moreover, all the foams have been compared with the material without space holder. Both materials show porosity in samples without space holder: 10 % and 32%, for  $Ti_2AlC$  and  $Ti_3SiC_2$  respectively as a consequence of the processing parameters. This porosity appears in the cell walls of all processed foams and such porosity can be tuned by variations on pressing and sintering conditions. This effect results in bimodal porosity in the foams.

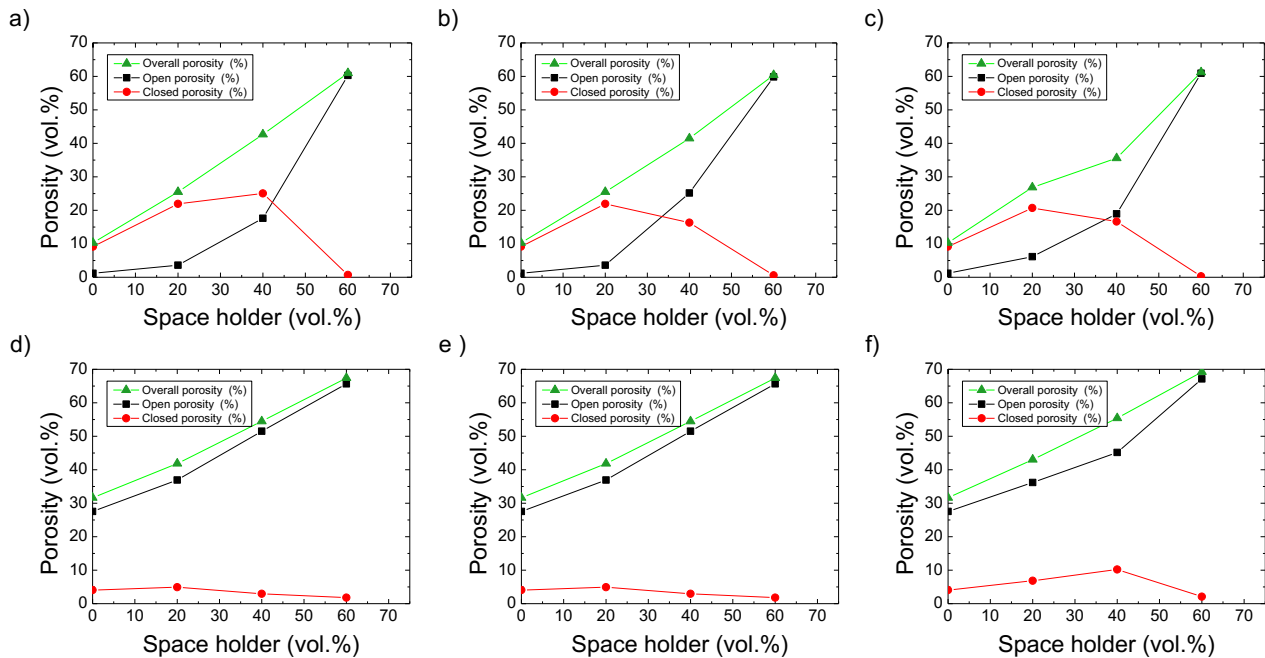


Figure 2. Variation of closed, open and overall porosity (vol.%) with the space holder (vol.%) added in the powder mixture for: a)  $Ti_2AlC$  and 250-400  $\mu m$  of space holder size distribution, b)  $Ti_2AlC$  and 400-800  $\mu m$  of space holder size distribution; c)  $Ti_2AlC$  and 800-1000  $\mu m$  of space holder size distribution; d)  $Ti_3SiC_2$  and 250-400  $\mu m$  of space holder size distribution, e)  $Ti_3SiC_2$  and 400-800  $\mu m$  of space holder size distribution; f)  $Ti_3SiC_2$  and 800-1000  $\mu m$  of space holder size distribution.

Figure 3 shows representative micrographs of foams for both materials at different magnifications. Figures 3a and 3b show the porosity of the cell walls for  $Ti_2AlC$  and  $Ti_3SiC_2$  respectively.  $Ti_3SiC_2$  shows higher cell wall porosity and more interconnected pores, which is in agreement with the porosity measurement results that show a much higher porosity in  $Ti_3SiC_2$  without space holder, as compared to Talc without space holder. This higher cell wall porosity might be responsible for the easier space holder dissolution observed in this foam. Representative microstructures of the foams are shown in figures 3c and 3d for both materials. It can be seen that pore morphology and distribution is similar and homogenous both materials. Overall appearance of the samples (figures 3e and 3f) is also similar and confirms that foams are well consolidated and easy to machine.

The comparison between overall and the theoretical porosity, namely that created only by addition of space holder, is shown in figures 4a and 4b for  $Ti_2AlC$  and  $Ti_3SiC_2$  respectively. For  $Ti_2AlC$  overall and theoretical porosity are similar, suggesting that most of the porosity is due to the addition of the space holder.  $Ti_3SiC_2$  presents more differences between theoretical and observed porosity due to the fact that the foam cell walls present higher level of porosity. The bimodal porosity present in the foams is represented as: Mode 1, which is the cell wall porosity, related to the processing parameters and Mode 2, which is the porosity created due to the addition of space holder. For both materials, overall porosity tends to be closer to the theoretical one as the amount of space holder increases. This occurs because the porosity contribution from the foam walls (Mode 1) decreases as the solid area decreases with increasing porosity.

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Table 2 shows the linear fitting for overall porosity variation with respect to the amount of the space holder for both materials and for each size distribution. The equations show the variation of the porosity with the space holder obeys a linear relationship with an accurate adjustment,  $R^2$ . These equations allow the determination the space holder needed to process foams with a specific porosity.

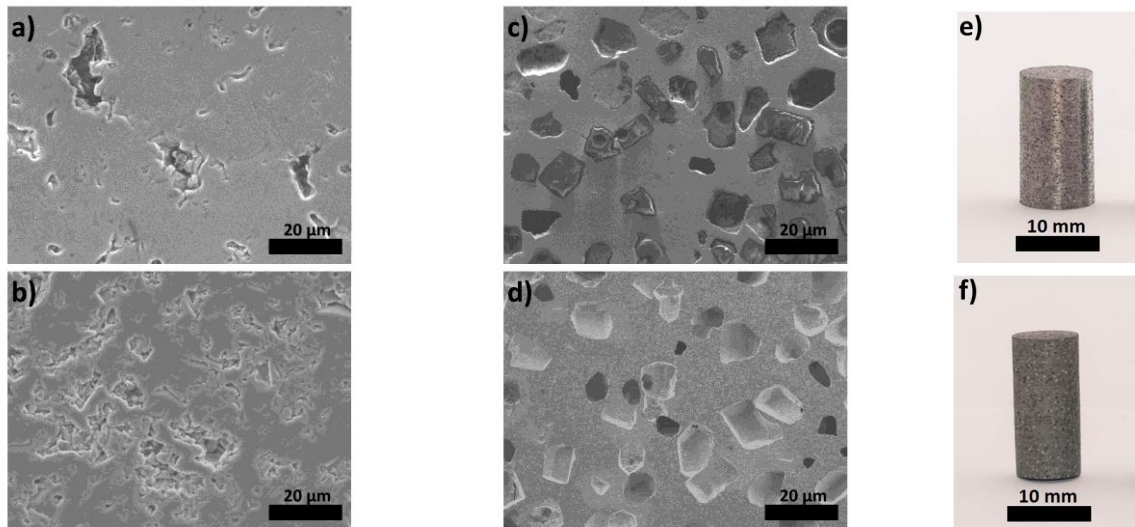


Figure 3. Representative microstructural features of foams of both materials (containing 40 vol.% and with 250-400 µm space holder size distribution) in three different magnifications: a) detail of cell wall for  $Ti_2AlC$  foam; b) detail of cell wall for  $Ti_3SiC_2$  foam; c) characteristic foam microstructure for  $Ti_2AlC$  foam; d) characteristic foam microstructure for  $Ti_3SiC_2$  foam; e)  $Ti_2AlC$  foam; f)  $Ti_3SiC_2$  foam.

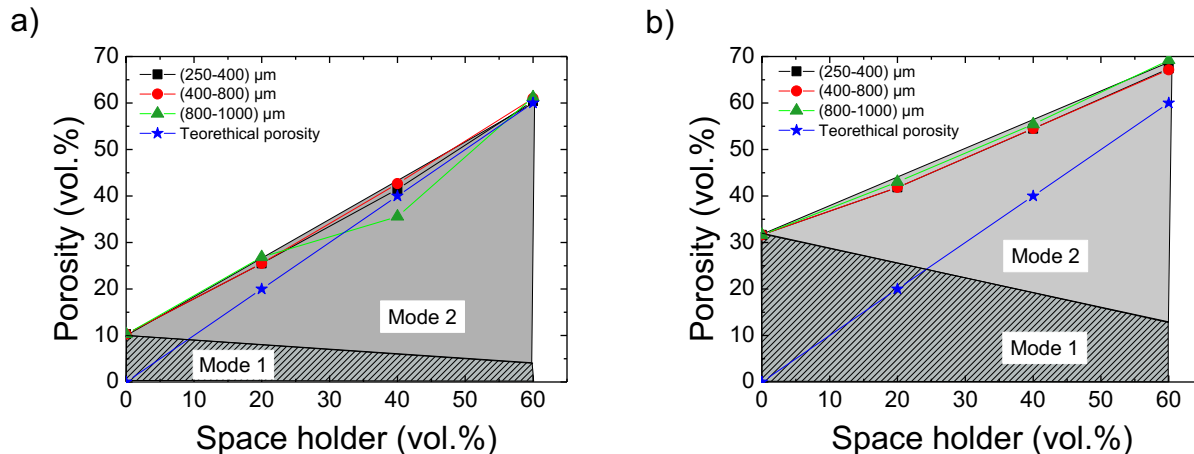


Figure 4. Variation of overall porosity (vol.%) with the addition of space holder (vol.%) in the mixture for the three space holder distributions (250-400 µm, 400-800 µm, and 800-1000 µm) for a)  $Ti_2AlC$  and b)  $Ti_3SiC_2$ . Moreover, both graphs distinguish the bimodal porosity: Mode 1: cell wall porosity and Mode 2: porosity due to the space holder.

Table 3 shows the gas permeability results for  $Ti_2AlC$  and  $Ti_3SiC_2$  respectively for the three space holder size distributions. Both materials show increase in permeability with increasing porosity. Previous studies have demonstrated [26, 27], that porosity is the parameter with most influence on the permeability. This study has shown that the addition of space holder generates open porosity. For  $Ti_2AlC$  permeability is shown for porosity values higher than 35.57 vol.% since it was not possible to measure samples with lower porosities due to high overpressure. Samples with porosity lower than 35.57 vol.% have mainly closed porosity therewith, the gas flow through the sample is 0 and the gas permeability should be approximately 0 too. In  $Ti_3SiC_2$  foam permeability is shown for all the samples since all of them have mainly open porosity.  $Ti_2AlC$  shows that for a fixed porosity (vol.%) the permeability is slightly higher for samples made with bigger space holder size distributions. The bigger space holder size leads to bigger pore sizes in the foam and increasing pore size increases the permeability [28].  $Ti_3SiC_2$  does not show clear tendency with the space holder size distribution.  $Ti_2AlC$  shows slightly higher permeability than  $Ti_3SiC_2$  for the same porosity values. There are several parameters which affect to the permeability, the

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most important are: porosity volume percentage, specific area and tortuosity. To get more conclusions about these results, specific area and tortuosity must to be determined and studied.

Table 2. Linear relationship between the overall porosity (vol.%) the addition of space holder (vol.%, x, for three different size distributions and the quadratic adjustment  $R^2$ . Results for:  $Ti_2AlC$  and  $Ti_3SiC_2$  materials.

Material	Space holder size distribution ( $\mu m$ )	Equation	$R^2$
$Ti_2AlC$	250-400	$y=0.8204x+10$	0.9971
	400-800	$y=0.8349x+10$	0.9980
	800-1000	$y=0.7757x+10$	0.9815
$Ti_3SiC_2$	250-400	$y=0.6054x+32$	0.9964
	400-800	$y=0.5725x+32$	0.9951
	800-1000	$y=0.6054x+32$	0.9964

Table 3. Variation of gas permeability, k, with the addition of space holder in the mixture and the porosity present in the foam for three space holder size distributions: 250-400  $\mu m$ , 400-800  $\mu m$ , and  $\mu m$  and 800-1000  $\mu m$  for both materials  $Ti_2AlC$  and  $Ti_3SiC_2$ .

Material	Space holder (vol.%)	Space holder size distribution (250-400) $\mu m$		Space holder size distribution (400-800) $\mu m$		Space holder size distribution (800-1000) $\mu m$	
		Overall porosity (vol.%)	k ( $m^2$ )	Overall porosity (vol.%)	k ( $m^2$ )	Overall porosity (vol.%)	k ( $m^2$ )
$Ti_2AlC$	40	41.5	$2.3 \times 10^{-18}$	42.7	$6.8 \times 10^{-18}$	35.6	$6.0 \times 10^{-18}$
	60	60.4	6.3	61.0	3.8	61.3	7.4
$Ti_3SiC_2$	0	31.6	$2.0 \times 10^{-16}$	31.6	$2.0 \times 10^{-16}$	31.6	$2.0 \times 10^{-16}$
	20	41.9	$3.6 \times 10^{-16}$	41.7	$3.9 \times 10^{-16}$	43.0	$3.9 \times 10^{-16}$
	40	54.5	$1.2 \times 10^{-14}$	54.5	$1.2 \times 10^{-15}$	55.4	$8.4 \times 10^{-16}$
	60	67.4	1.2	67.2	1.4	69.2	2.2

## 4. CONCLUSIONS

This work has achieved consolidated foams with controlled porosity. Space holder dissolution was optimized achieving 100% and 93% of mass loss for  $Ti_2AlC$  and  $Ti_3SiC_2$  respectively. With the selection of space holder size distribution the pore size was modified while tuning the powder/space holder ratio the porosity percentage in the foam is controlled. The resulting porosity is bimodal: Mode 1 represents cell wall porosity and depends on the processing parameters and Mode 2 depends on the amount of space holder. The porosity created by the addition of space holder in the mixture has been fitted to a linear equation with accuracy of  $R^2$  of 0.99. The equation depends on the material and the space holder size distribution. The gas permeability has been studied on samples with mainly open porosity. The gas permeability depends on the porosity volume percentage, specific area and tortuosity.

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