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3 **Correlation between circuital current, Cu(II) reduction and cellular**  
4 **electron transfer in EAB isolated from Cu(II)-reduced biocathodes**  
5 **of microbial fuel cells**

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17

18 **Abstract**

19 The performance of four indigenous electrochemically active bacteria (EAB)  
20 (*Stenotrophomonas maltophilia* JY1, *Citrobacter* sp. JY3, *Pseudomonas aeruginosa*  
21 JY5 and *Stenotrophomonas* sp. JY6) was evaluated for Cu(II) reduction on the  
22 cathodes of microbial fuel cells (MFCs). These EAB were isolated from well  
23 adapted mixed cultures on the MFC cathodes operated for Cu(II) reduction. The  
24 relationship between circuital current, Cu(II) reduction rate, and cellular electron  
25 transfer processes was investigated from a mechanistic point of view using X-ray  
26 photoelectron spectroscopy, scanning electronic microscopy coupled with energy  
27 dispersive X-ray spectrometry, linear sweep voltammetry and cyclic voltammetry.  
28 JY1 and JY5 exhibited a weak correlation between circuital current and Cu(II)  
29 reduction. A much stronger correlation was observed for JY3 followed by JY6,  
30 demonstrating the relationship between circuital current and Cu(II) reduction for  
31 these species. In the presence of electron transfer inhibitors (2,4-dinitrophenol or  
32 rotenone), significant inhibition on JY6 activity and a weak effect on JY1, JY3 and  
33 JY5 was observed, confirming a strong correlation between cellular electron transfer  
34 processes and either Cu(II) reduction or circuital current. This study provides  
35 evidence of the diverse functions played by these EAB, and adds to a deeper  
36 understanding of the capabilities exerted by diverse EAB associated with Cu(II)  
37 reduction.

38

39 **Keywords:** biocathode; microbial fuel cell; electrochemically active bacteria; Cu(II)  
40 reduction; electron transfer inhibitor

41

## 42 **1 Introduction**

43 Microbial fuel cells (MFCs) are emerging as new, sustainable and effective  
44 technologies for the recovery of heavy metals from waste and wastewater [1].  
45 Among diverse heavy metals, Cu(II), which is common in the electroplating and  
46 mining industries [2-3], has attracted significant attention due to the potential for its  
47 recovery and simultaneous wastewater detoxification. The recovery of Cu(II) with  
48 abiotic cathode MFCs has been demonstrated over a wide range of operating  
49 conditions and cell architectures [4-9]. However, abiotic cathodes often require the  
50 use of costly noble or non-noble co-catalysts in addition to an acidic medium.  
51 Therefore, the development of biocathodic MFCs, which are based on the catalysis  
52 of self-regenerating electrochemically active bacteria (EAB) under a neutral  
53 environment, may provide a sustainable and green alternative to abiotic systems.  
54 Biocathodic MFCs avoid the use of expensive materials and toxic organic reagents,  
55 and reduce the consumption of energy and acids [10-14]. Biocathodes are also able  
56 to reduce electrode overpotentials, the production of sludge, and the overall cost and  
57 the maintenance of MFCs. MFCs, utilizing mixed cultures, have been shown to be  
58 efficient in the recovery of Cu(II) from mixed metal influent and also a promising  
59 system for the synthesis of copper [15]. In contrast, MFCs with biocathodes operated  
60 with pure cultures have been used to study specific EAB and their electrochemical  
61 performance [10-14]. The exogenous EAB of *Shewanella* is one of the few examples  
62 which is able to reduce a metal (Cr(VI)) in MFCs [16-17].

63 Microorganisms possess endurance to aqueous Cu(II) through a variety of  
64 mechanisms due to their intrinsic abilities and habitat sites [18-20]. Therefore, well  
65 adapted microorganisms could provide new insights with regards to heavy metal  
66 reduction in MFCs. A limited number of microorganisms exhibiting efficient rates of  
67 Cu(II) reduction have been cultivated under Cu(II)-adaptive conditions [20-24].  
68 Similar considerations, in principle, hold true for their use in cathodic reductive  
69 environments in MFCs, under which the activities of different indigeneous EAB may  
70 exhibit various Cu(II) reduction rates. In parallel, EAB immobilized on the surface  
71 of cathodes may also be able to utilize cathodic electrons for their internal  
72 metabolism [11,25]. The operation of MFCs at different concentrations of Cu(II) in  
73 the catholyte is expected to clarify the correlation between the circuital current and  
74 the rate of Cu(II) reduction associated with the use of isolated EAB.

75 The bacteriological reduction of Cu(II), in the absence of a circuital current, is  
76 believed to be associated with cellular electron transfer processes through the  
77 cytoplasmic membrane and with the flux of protons through ATP-synthase [26-27].  
78 Such mechanisms can be unravelled using cellular electron transfer inhibitors, such  
79 as 2,4-dinitrophenol (DNP) and rotenone (C<sub>23</sub>H<sub>22</sub>O<sub>6</sub>). DNP dissipates the proton  
80 motive force associated with cellular electron transfer processes, and decreases  
81 hydrogen production by inhibiting the ATP synthesis by photophosphorylation, in  
82 the absence of a circuital current [28]. In contrast, rotenone inhibits the activity of  
83 NADH-dehydrogenase and blocks the reduction of U(VI) by facultative anaerobic  
84 bacteria in the absence of a circuital current [29]. The utilization of rotenone and  
85 DNP, in the presence and absence of a circuital current passing through the EAB

86 cathodes of MFCs is thus expected to establish whether the circuital current and  
87 Cu(II) reduction are associated with cellular electron transfer processes in the EAB  
88 species.

89 In this study, we elucidate from a mechanistic point of view the performance  
90 and impact of four indigenous different EAB on Cu(II) reduction in MFCs. The EAB  
91 tentatively identified as *Stenotrophomonas maltophilia* JY1, *Citrobacter* sp. JY3,  
92 *Pseudomonas aeruginosa* JY5 and *Stenotrophomonas* sp. JY6, were isolated from  
93 well adapted mixed cultures grown on the surface of MFC cathodes operated for  
94 Cu(II) reduction [15]. X-ray photoelectron spectroscopy (XPS), scanning electronic  
95 microscopy (SEM) coupled with energy dispersive X-ray spectrometry (EDS), linear  
96 sweep voltammetry (LSV) and cyclic voltammetry (CV) were used to investigate the  
97 effect of circuital current on the speciation of the deposited copper, the morphologies  
98 of the cathodes and the cathodic redox reactions for each EAB species. The  
99 relationship between circuital current, the rate of Cu(II) reduction and the cellular  
100 electron transfer processes associated with each of the four EAB were clarified  
101 through the system response to a step change of Cu(II) concentration in the catholyte  
102 and reaction mechanisms elucidated in the presence or absence of DNP or rotenone  
103 electron transfer inhibitors.

104

## 105 **2 Materials and Methods**

### 106 *2.1 EAB isolation, incubation and identification*

107 Bacterial isolates were obtained from mixed culture cultivated in the  
108 Cu(II)-reduced biocathodes of MFCs [15]. The isolation and incubation processes  
109 are detailed in the Supplementary Material (SM). The DNA of these EAB isolates  
110 was extracted using a Qubit2.0 DNA kit (Sangon Biotech (Shanghai) Co. Ltd., China)  
111 according to the manufacturer's procedure. The 16S rRNA gene was amplified by  
112 PCR using universal primers 518 F (5' CAGAGTTTGATCCTGGCT3') and 1540R  
113 (5'AGGAGGTGATCCAGCCGCA3'), as described in SI. The sequence data were  
114 compared with the GenBank database using the Blast server at NCBI  
115 (<http://www.ncbi.nlm.nih.gov/BLAST/>) to accurately identify the bacterial strains.  
116 All tests were performed in duplicate.

117

### 118 *2.2 MFC reactors setup and operation*

119 Identical two-chamber MFCs with cylindrical chambers 4.0 cm long by 3.0 cm  
120 in diameter were used in all experiments. The anodic and cathodic chambers were  
121 separated by a cation exchange membrane (CEM) (CMI-7000 Membrane  
122 International, Glen Rock, NJ) with a projected surface area of 7.1 cm<sup>2</sup>. Both the  
123 anode and cathode were filled with graphite felt (1.0 cm × 1.0 cm × 0.5 cm, 8 pieces,  
124 Sanye Co., Beijing, China) and carbon rods were used as current collectors in both  
125 anode and cathode. For each of the duplicate reactors three replicate experiments  
126 were performed. The MFCs were operated at a fixed external resistance of 510 Ω.

127 The anodes were inoculated with suspended bacteria collected from a previous  
128 acetate-fed MFC reactor and an equivalent volume of nutrient solution containing  
129 acetate (1.0 g/L) was added [30-31]. The cathodes were fed using the same medium,

130 except acetate was replaced by NaHCO<sub>3</sub> (10 mg/L), with further addition of Cu(II)  
131 (5 mg/L) to the cathodic chambers. Cathodes were quantitatively inoculated with the  
132 isolates with a total of  $3 \times 10^8$  colony forming unit. The anolyte and catholyte were  
133 sparged with N<sub>2</sub> gas for 15 min prior to adding the solutions into the electrode  
134 chambers. No measurable Cu(II) in the anolyte and acetate in the catholyte were  
135 observed during each cycle operation, excluding the possibility of Cu(II) and acetate  
136 diffusion between the chambers, although the retention of Cu(II) on the ion  
137 exchange membrane could not be precluded [15]. Other catholyte and operational  
138 conditions are described in SM.

139 The performance of the biocathodes was evaluated against four control  
140 experiments, including (i) the operation of the reactors under the open circuit  
141 condition (OCC), (ii) the operation with a closed circuit but without the inoculation  
142 of the EAB (abiotic control), (iii) the cathodes covered with the EAB but in the  
143 absence of Cu(II), and (iv) the cathodes tested in the absence of both EAB and  
144 Cu(II). The last two control experiments were used to evaluate the CVs performance  
145 of the cell.

### 147 2.3 Measurement, analysis and calculation

148 The circuit current, dissolved oxygen, biomass, organics and Cu(II)  
149 concentration were determined according to the methodology reported in SM. The  
150 rate of Cu(II) removal and charge distribution were calculated as detailed in SM.

151 Maximum power was obtained by running LSV at a scan rate of 0.1 mV/s  
152 [30-31]. Power and current densities were normalized to the projected surface area of  
153 the membrane. EAB cathode redox behavior was studied using CV (CHI 650,  
154 Chenhua, Shanghai). The potential was scanned between -0.36 V and +0.46 V (vs  
155 SHE) at a scan rate of 1.0 mV/s using a standard three-electrode arrangement with the  
156 biocathode as the working electrode, platinum plate as the counter electrode, and  
157 Ag/AgCl as the reference electrode. One-way ANOVA in SPSS 19.0 was used to  
158 analyze the statistical variation of the data, and all of the data indicated significance  
159 levels of  $p < 0.05$ .

160 The surfaces of the Cu-laden biomass were analyzed by X-ray photoelectron  
161 spectroscopy (XPS, Thermo Fisher Scientific, ESCALAB 250, US) with a Mono Al  
162 K $\alpha$  X-ray source (1486.6 eV of photons). The X-ray source was run at a reduced  
163 power of 150 W. The morphology of the electrodes after Cu(II) reduction were  
164 examined with a SEM (QUANTA450, FEI company, USA) equipped with an EDS  
165 (X-MAX 20 mm<sup>2</sup>/50 mm<sup>2</sup>, Oxford Instruments, UK) according to the method  
166 described previously [15,30].

## 168 3 Results and Discussion

### 169 3.1 EAB Isolation

170 Four EAB were successfully isolated from well adapted mixed cultures grown on  
171 the surface of MFC cathodes operated for Cu(II) reduction [15] (Table S1). All  
172 bacteria were gram-negative and major opportunistic to facultative or survived from  
173 an anaerobic environment. JY1 matching *Stenotrophomonas maltophilia*, is known to

174 convert Cu(II) into Cu(0) on the cell surface, in the absence of cathodic electrons  
175 [22-24]. *S. maltophilia* has been isolated previously from a copper polluted area [22],  
176 and has never been reported in MFCs. JY3 closely related to *Citrobacter* sp., is able to  
177 remove Cu(II) in a medium of  $\text{SO}_4^{2-}$  through the formation of CuS precipitate in the  
178 absence of cathodic electrons [20]. It has been isolated previously from anodic MFC  
179 biofilms in the absence of Cu(II) [32]. JY5 matching *Pseudomonas aeruginosa*, is  
180 able to remove Cu(II) in the absence of cathodic electrons [21]. It has been reported in  
181 either denitrification autotrophic biocathodes of MFCs [33], or in MFCs operated for  
182 the degradation of phenol and glycerol through mediated electron transfer [34-37].  
183 Finally, JY6 corresponding to *Stenotrophomonas* sp., can tolerate high concentrations  
184 of metals including Ag, Cu, Cd, Hg and Mn [38-39] and has been isolated previously  
185 from a wide range of environments.

186

### 187 3.2 EAB activity assessment

188

#### Here Fig. 1

189 All four EAB played a significant role in the reduction of Cu(II) in the MFCs and  
190 displayed rates of Cu(II) reduction higher than those found in both OCC and abiotic  
191 CCC controls (Fig. 1A). Previous studies with mixed culture biocathodes using  
192 nitrobenzene, pentachlorophenol, Cr(VI), Co(II) or Cu(II) as an electron acceptor  
193 [31,40-44] support these findings. The Cu(II) reduction rates in the range  $(0.82 \pm 0.05$   
194  $- 1.11 \pm 0.01 \text{ mg/L/h})$  were close to those found in mixed cultures  $(1.07 \pm 0.01$   
195  $\text{mg/L/h})$  at the same Cu(II) concentration (5 mg/L) [15], reflecting the robust capacity  
196 of these isolates for reducing Cu(II).

197

#### Here Fig. 2

198 The results in Figs. 1 and 2 show that the EAB catalytic process produced higher  
199 circuital currents (Fig. 1B), open circuit potentials (Fig. 2A and B) and maximum  
200 power production (Fig. 2C and D) in comparison with the values under abiotic control,  
201 irrespective of the Cu(II) concentrations of 5 mg/L (Figs. 1, 2A and 2C) and 20 mg/L  
202 (Figs. 1, 2B and 2D). The background circuital current, voltage output, power  
203 production and electrode potential in the absence of Cu(II) (Figs. 1B, 2A and 2C, and  
204 Fig. S1) were attributed to the reduction of residual dissolved oxygen [15,43].

205 Higher circuital currents and rates of Cu(II) reduction were observed by  
206 increasing the concentration of Cu(II) in the cathodic chamber from 5 mg/L to 20  
207 mg/L (Fig. 1). This effect was more significant for JY3 and JY6, demonstrating the  
208 significant impact of circuital current on the rate of Cu(II) reduction for these two  
209 species. Conversely, the circuital currents observed with JY1 and JY5 were  
210 insignificant (Fig. 1B), in relation to the significant increase observed in the rate of  
211 Cu(II) reduction (Fig. 1A). The reduction of Cu(II) can therefore be ascribed to the  
212 effect of the abiotic cathodes only and to the effect of the individual JY1 or JY5  
213 bacteria in response to the increase in Cu(II) concentration (Fig. 1A). These results  
214 illustrate the weak correlation between circuital current and the rate of Cu(II)  
215 reduction for both JY1 and JY5, a result that will be further supported by the XPS



216 analyses.

217 The majority of the EAB cathodes displayed significant overshoots in voltage  
218 output and power density in comparison with the abiotic controls, at a Cu(II)  
219 concentration of 20 mg/L (Fig. 2B and D). This suggests that the demand for electrons  
220 in these experiments exceeded the rate of electrons supplied by microbial activity, and  
221 this resulted in the depletion of electrons and ions in the catholyte. Such observations  
222 have also been reported in other MFC studies using O<sub>2</sub> as electron acceptor [45-47].  
223 The cathode with bacterial JY3 displayed the highest performance with the highest  
224 circuital current (Fig. 1B) and most importantly without displaying an overshoot in  
225 power density, indicating that the microbial activity with this species was significant.

226 The cathodic potentials of all EAB were found to vary much more than the  
227 anodic potentials, over the current density range investigated (Fig. S2A, initial Cu(II)  
228 of 5 mg/L; Fig. S2B, initial Cu(II) of 20 mg/L). In consequence, the performance of  
229 the MFCs was controlled by the reduction of copper at the biocathode, rather than the  
230 microbial phenomena that occurred at the anode. The presence of the EAB at the  
231 cathode, therefore, had a significant impact on the propensity of the cathodes for  
232 electricity generation and voltage output.

233 Increasing the concentration of Cu(II) in the catholyte diverted a larger fraction  
234 of electrons from the anodic oxidation of organics towards the reduction of Cu(II),  
235 with JY6 showing the highest value among the different EAB ( $11.2 \pm 0.1\%$  from a  
236 total of 2.9 C and at a Cu(II) of 20 mg/L). The remaining  $0.4 \pm 0.0\%$  was used for  
237 oxygen reduction,  $52.3 \pm 0.0\%$  for organics production, and  $33.5 \pm 0.0$  for biomass  
238 growth (Table S2). A large fraction of the cathodic electrons from  $2.6 \pm 0.1\%$  for JY6  
239 up to  $43.2 \pm 0.4$  for JY3 were involved in other parallel reactions or unknown  
240 processes.

241 The abiotic cathodes displayed reductive peak potentials of 0.033 V at a Cu(II)  
242 of 5 mg/L (Fig. S3A and Table S3) and 0.037 V at 20 mg/L (Fig. S3B and Table S3),  
243 reflecting the positive shift of reductive peak potential at a higher Cu(II)  
244 concentration. Reductive onset potentials for all EAB cathodes were more positive  
245 than the abiotic controls ( $0.272 - 0.297$  V vs. 0.264 V at a Cu(II) of 5 mg/L and  
246  $0.278 - 0.328$  V vs. 0.267 V at a Cu(II) of 20 mg/L) (Table S3) and the shift was  
247 more significant for the reductive peak potentials of all EAB cathodes with respect  
248 to the abiotic controls ( $0.040 - 0.063$  V vs. 0.033 V at a Cu(II) of 5 mg/L,  $0.043 -$   
249  $0.079$  V vs. 0.037 V at a Cu(II) of 20 mg/L). These results, in combination,  
250 demonstrate the varying degree of influence exerted by each EAB on the catalytic  
251 activity toward Cu(II) reduction, which is consistent with the effect of EAB on the  
252 reduction of Co(II) and chloramphenicol on mixed culture cathodes [43,48]. The JY1  
253 and JY5 bacteria exhibited much lower reductive onset potentials than JY3 and JY6,  
254 implying a weaker interaction between cathodic electrons and the reduction of Cu(II)  
255 through the mediation of these two species.

256 The reductive peak currents, at a Cu(II) concentration of 5 mg/L, observed on  
257 the cathodes covered by the EAB were lower than values registered with the abiotic  
258 cathode (0.973 mA) with the exception of JY6 (Table S3), suggesting some degree  
259 of mass transfer inhibition for Cu(II) due to the contact between the EAB and the

260 electrode surface [47]. At a higher concentration of Cu(II) (20 mg/L), the mass  
261 transfer inhibition became less significant, as expected. Similar observations have  
262 been reported for the reduction of other electron acceptors such as Cr(VI) and Co(II)  
263 in mixed culture cathodes [41,43].

264 The lack of a significant difference observed between CVs of the abiotic controls  
265 and the biotic cathodes in the absence of Cu(II) (Fig. S4), in concert, reflected the  
266 importance of Cu(II) ions on the occurrence of reduction reactions on the EAB,  
267 despite the expected variability due to the redox species present on the surfaces of  
268 these EAB cells (Insets in Fig. S4).

269

### 270 3.3 Electrode morphology and product analysis

271 SEM examination showed that the EAB covered the surface of the cathodes only  
272 sparsely (Fig. S5A, D, G, and J). EDS analysis confirmed the presence of Cu  
273 precipitates on the surfaces of EAB cells (Fig. S5B, E, H and K) while no Cu, or very  
274 little Cu precipitate, was observed on the bare surface of the electrodes (Fig. S5C, F, I  
275 and L). EDS detection of carbon, oxygen, sodium and phosphorus was attributed to  
276 the cellular components of EAB on the electrodes, while gold was associated with the  
277 sample pretreatment.

278 XPS analyses (Fig. S6) indicated that the whole Cu2p region comprises 2p<sub>1/2</sub>  
279 and 2p<sub>3/2</sub> peaks, while only the Cu2p<sub>3/2</sub> peaks could be used for the assignment of  
280 copper chemical states [49]. The abiotic control reported the exclusive presence of  
281 Cu(0) (Fig. S6A), shown with its characteristic peak at the Cu2p<sub>3/2</sub> region of 932.4  
282 eV [49], while under OCC only adsorbed Cu(II) was observed (Fig. S6B), as expected.  
283 This result clearly demonstrates the importance of the effect of circuital current on the  
284 reduction of Cu(II) to Cu(0) with the abiotic cathodes.

285

### Here Fig. 3

286 The XPS analysis on the EAB cathodes in the presence of a circuital current (Fig.  
287 3), reported the exclusive presence of Cu(0), while under OCCs, both Cu(0) and Cu(II)  
288 were observed for JY1 (Fig. 4A) and JY5 (Fig. 4C), and only Cu(II) for both JY3 (Fig.  
289 4B) and JY6 (Fig. 4D). JY5 had a net Cu(0) production of  $1.81 \pm 0.11$  mg and JY1  
290 exhibited a  $1.45 \pm 0.05$  mg, both of which were nearly equivalent to the sum of  $1.17 \pm$   
291  $0.07$  mg in the abiotic controls and  $0.70 \pm 0.09$  mg (JY5) or  $0.44 \pm 0.03$  mg (JY1) in  
292 the absence of a circuital current (Table S4). These results in concert confirm the  
293 weak correlation between circuital current and the rate of Cu(II) reduction for both  
294 JY1 and JY5, which is consistent with the results shown in Fig. 1. The observation of  
295 Cu(0) in JY1 in the absence of a circuital current is consistent with previous studies,  
296 where *S. maltophilia* converted Cu(II) into Cu(0) under facultative conditions [22-24].

297

### Here Fig. 4

298

### 299 3.4 Effect of electron transfer inhibitors (rotenone and DNP)

300

### Here Fig. 5

301 In the presence of either rotenone or DNP, the rate of Cu(II) reduction (Fig. 5A)  
302 or the circuital current (Fig. 5B) registered in the MFCs with JY1 or JY5 EAB,  
303 changed little, suggesting a weak correlation between the cellular electron transfer  
304 processes and either Cu(II) reduction or the circuital current. Conversely, the cathode  
305 with the JY6 species, returned an appreciable decrease in both the rate of Cu(II)  
306 reduction and circuital current, suggesting a strong interaction between the cellular  
307 electron transfer processes in JY6 and either Cu(II) reduction or circuital current. This  
308 strong interaction observed with JY6 rather than with JY1, JY3 and JY5, was also  
309 supported by the apparent decrease in cathodic electrons used for Cu(II) reduction in  
310 the former, in the presence of rotenone or DNP, while little change in was observed  
311 with the other three EAB (Table S2). The negative effects of rotenone or DNP  
312 electron transfer inhibitors on JY6 was also reflected by a decrease in the voltage  
313 output (Fig. S7A and B), maximum power density (Fig. S7C and D) and cathode  
314 potential (Fig. S7E and F), in addition to the negative shifts observed in reductive  
315 onset potential, reductive peak potential and reductive peak current (Table S3; Fig.  
316 S8). In contrast, little change on the above characterization parameters was observed  
317 for JY1, JY3 and JY5. These results further support the weak dependence between the  
318 cellular electron transfer processes and either Cu(II) reduction or circuital current for  
319 JY1, JY3 and JY5, and confirm the significant correlation observed between the  
320 cellular electron transfer processes and either Cu(II) reduction or circuital current for  
321 JY6. The findings of this study are summarized graphically in Fig. 6.

322 **Here Fig. 6**

#### 323 **4 Conclusions**

324 Metal reduction in MFCs is known to be dependent upon the availability of  
325 cathodic electrons and upon the composition of bacterial communities on the  
326 biocathodes [11,15,40]. On the basis of the results obtained with indigenous EAB JY1,  
327 JY3, JY5 and JY6 isolated from well adapted mixed cultures grown on the surface of  
328 MFC cathodes used for Cu(II) reduction, this study demonstrates the close correlation  
329 among circuital current, the rate of Cu(II) reduction and the cellular electron transfer  
330 processes for JY6, and the weak dependence of these for JY1 and JY5 (Fig. 6). We  
331 therefore suggest the possibility of a mechanism involving direct electron transfer  
332 from the surfaces of the cathodes to JY6, followed by the subsequent cellular electron  
333 transfer to Cu(II) for its reduction. This mechanism is not reflected in JY3, which only  
334 exhibited a close correlation between circuital current and the rate of Cu(II) reduction  
335 (Fig. 6). In summary, this study provides an evidence of the diverse functions played  
336 by these EAB species in the mixed cultures and the corresponding effect on MFC  
337 characterization parameters. The results in this study add to a deeper understanding of  
338 the capabilities exerted by diverse EAB associated with Cu(II) reduction, and provide  
339 new insights into the potential application of metallurgical biocathode MFCs for Cu(II)  
340 recovery at industrial scale.

341

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502 **Figure captions**

503 **Fig. 1** Comparison of Cu(II) removal rate (A) and circuit current (B) with various  
504 EAB at an initial Cu(II) of either 5 mg/L or 20 mg/L.

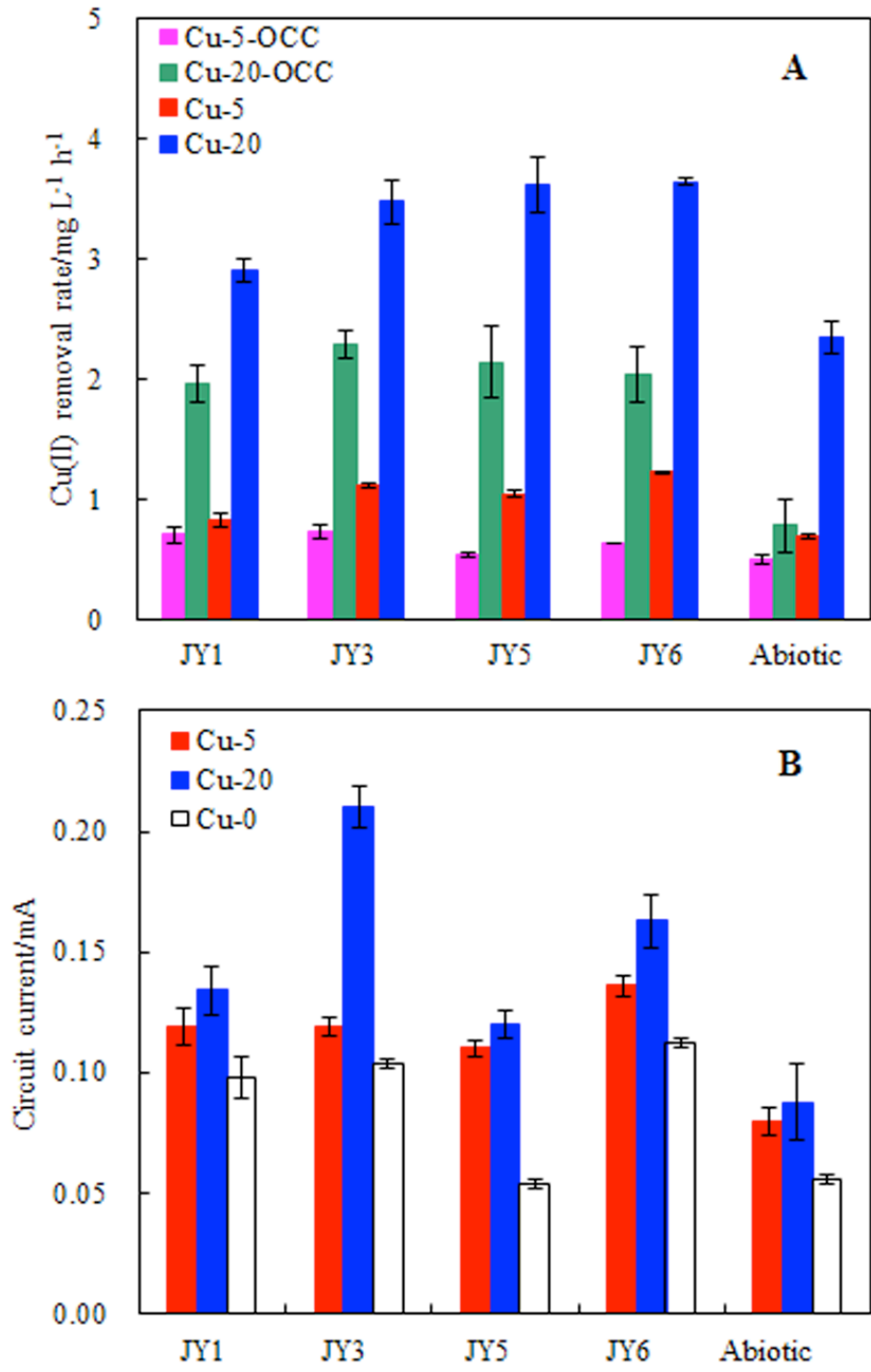
505 **Fig. 2** Voltage output (A and B), power density (C and D) as a function of current  
506 density with various EAB at an initial Cu(II) of 5 mg/L (A and C) or 20 mg/L (B and  
507 D).

508 **Fig. 3** XPS spectra of Cu precipitates on the cathodes catalyzed by EAB of JY1 (A),  
509 JY3 (B), JY5 (C) or JY6 (D) (initial Cu(II): 20 mg/L; 20 batch cycles).

510 **Fig. 4** XPS spectra of Cu precipitates on the cathodes catalyzed by EAB of JY1 (A),  
511 JY3 (B), JY5 (C) or JY6 (D) in the absence of circuit current (initial Cu(II): 20  
512 mg/L; 20 batch cycles).

513 **Fig. 5** Comparison of Cu(II) removal rate (A) and circuit current (B) in response to  
514 the inhibitor of rotenone or DNP (initial Cu(II): 20 mg/L).

515 **Fig. 6** Summary of correlation between circuit current, Cu(II) reduction and cellular  
516 electron transfer in EAB of JY1, JY3, JY5 and JY6.



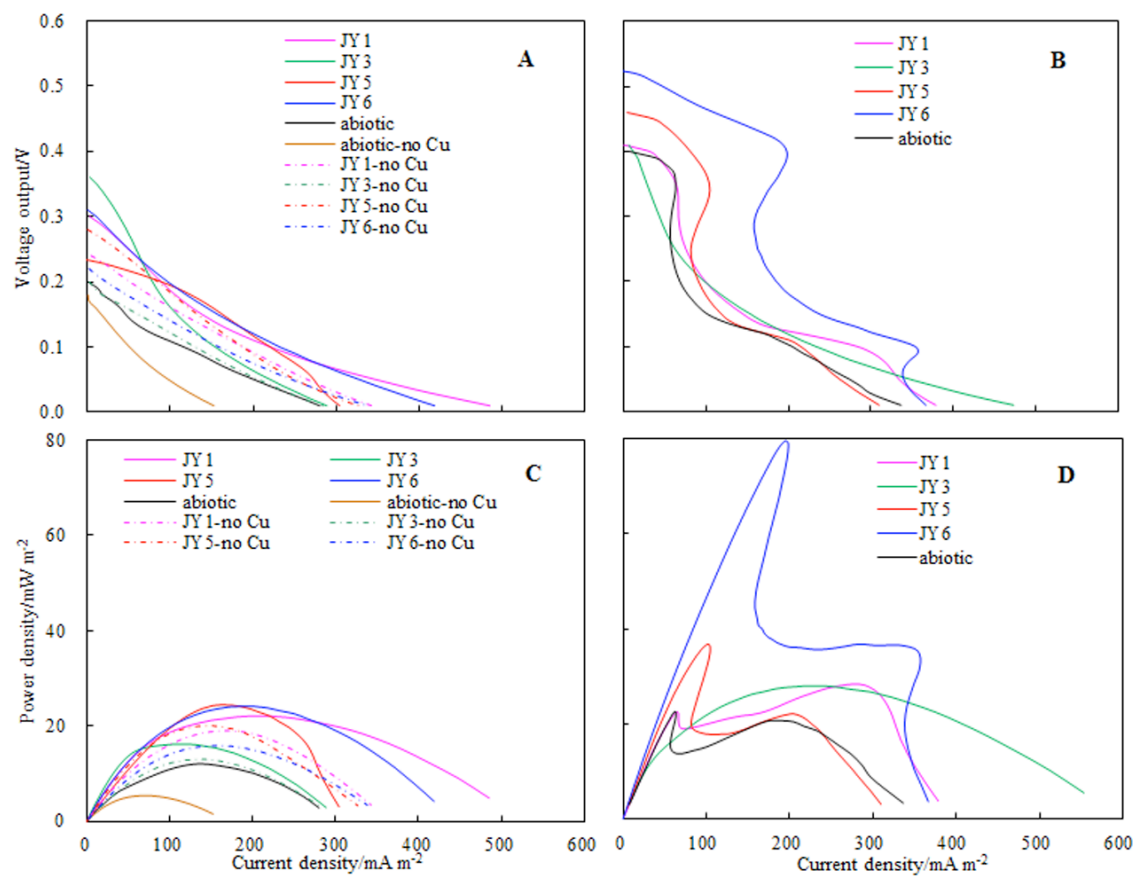
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519 Figure 1

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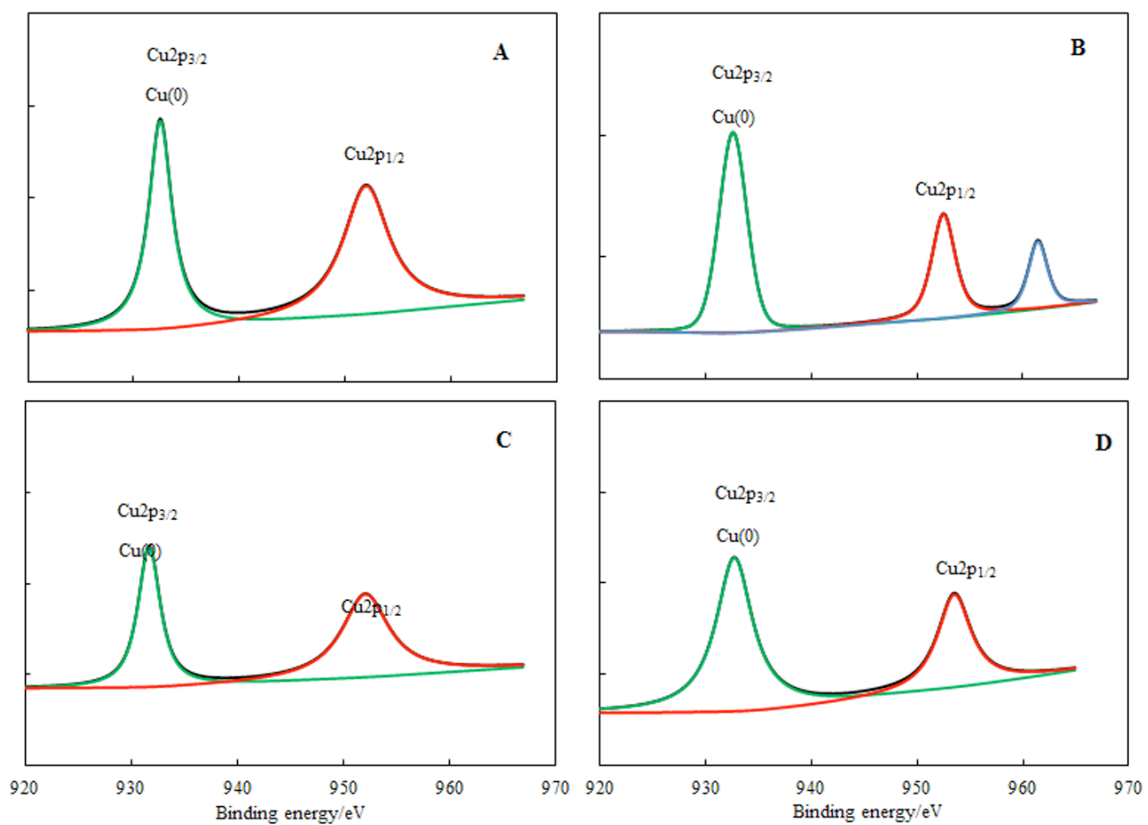




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522 **Figure 2**

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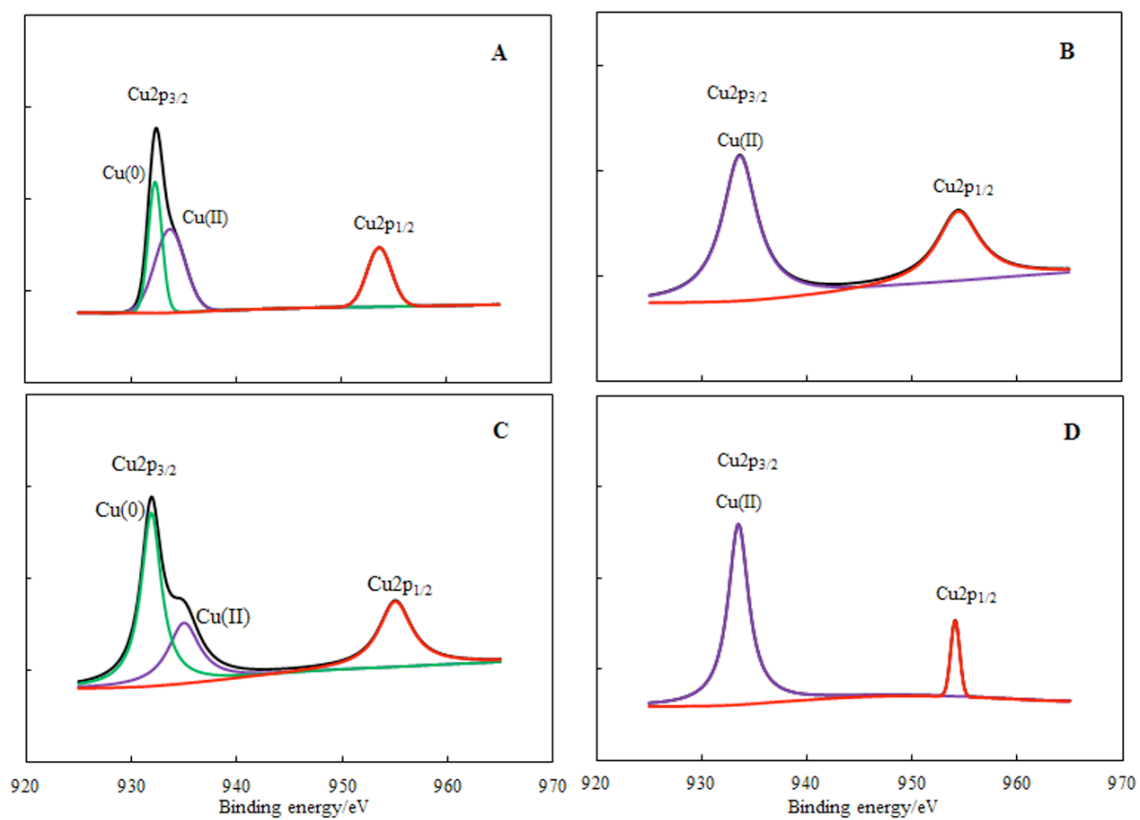


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Figure 3

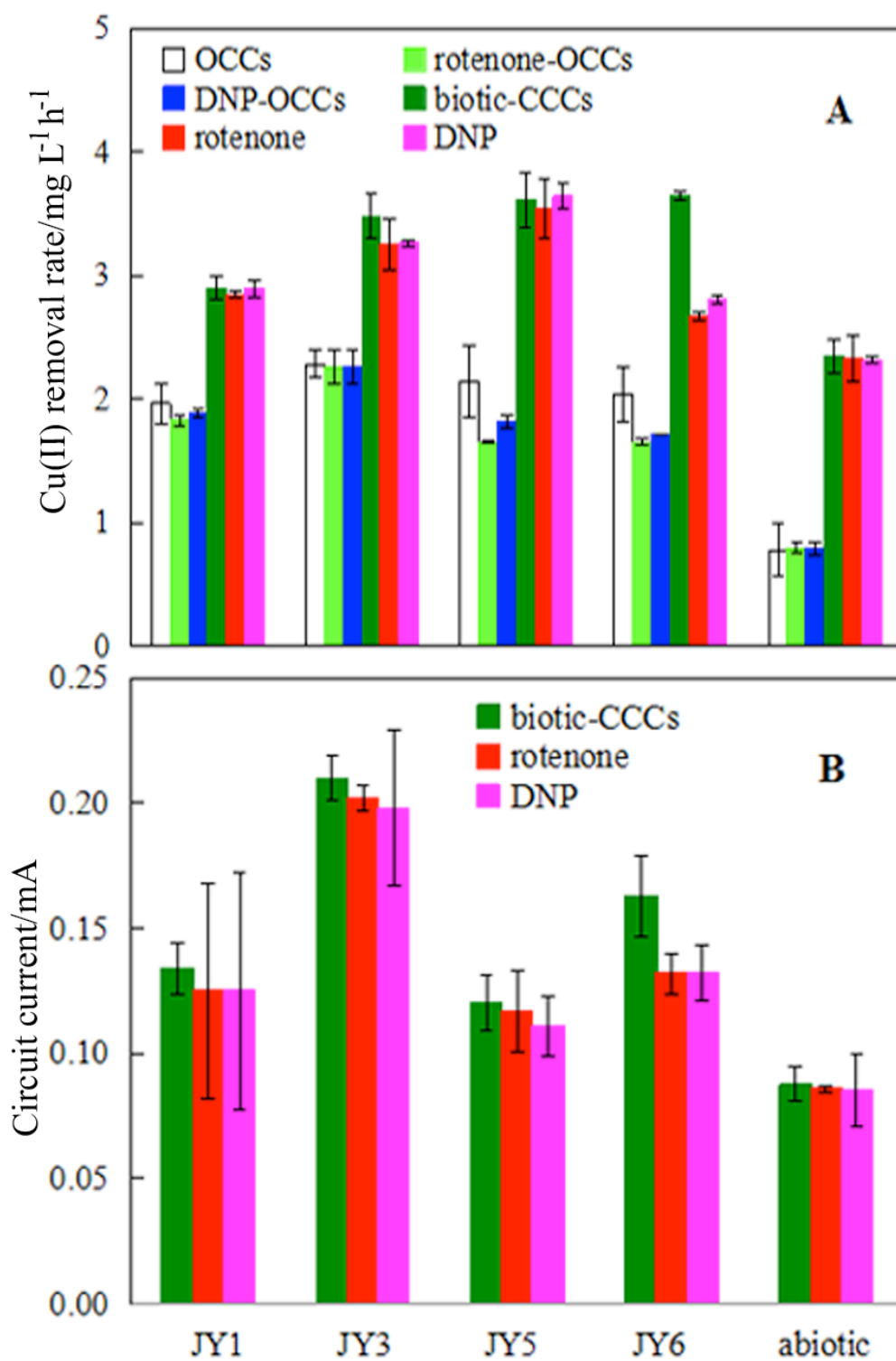
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528 Figure 4

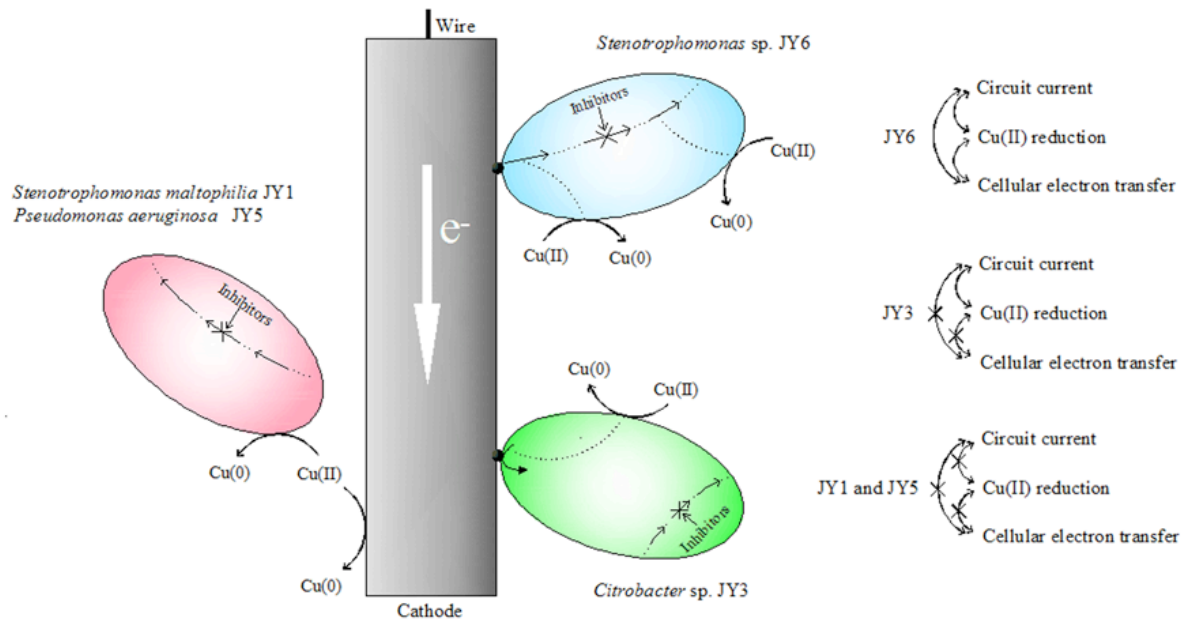
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531 Figure 5

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535 Figure 6