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Abstract: Kinetics of spreading of mixed solutions of cationic and anionic surfactants over highly hydrophobic substrate such as polyethylene is investigated. It is shown that due to synergetic effect these solutions can wet hydrophobic substrates nearly as effective as solutions of trisiloxane superspreader BT-278. The spreading factor reaches 70 % of that of superspreader for the most effective mixed solution. At room humidity (40 %) spread area has a maximum vs concentration. However, the maximum was not observed at higher humidity 80 %. The spreading rate of mixed solutions is smaller than that of superspreader despite the same spreading exponent $n=0.5$.

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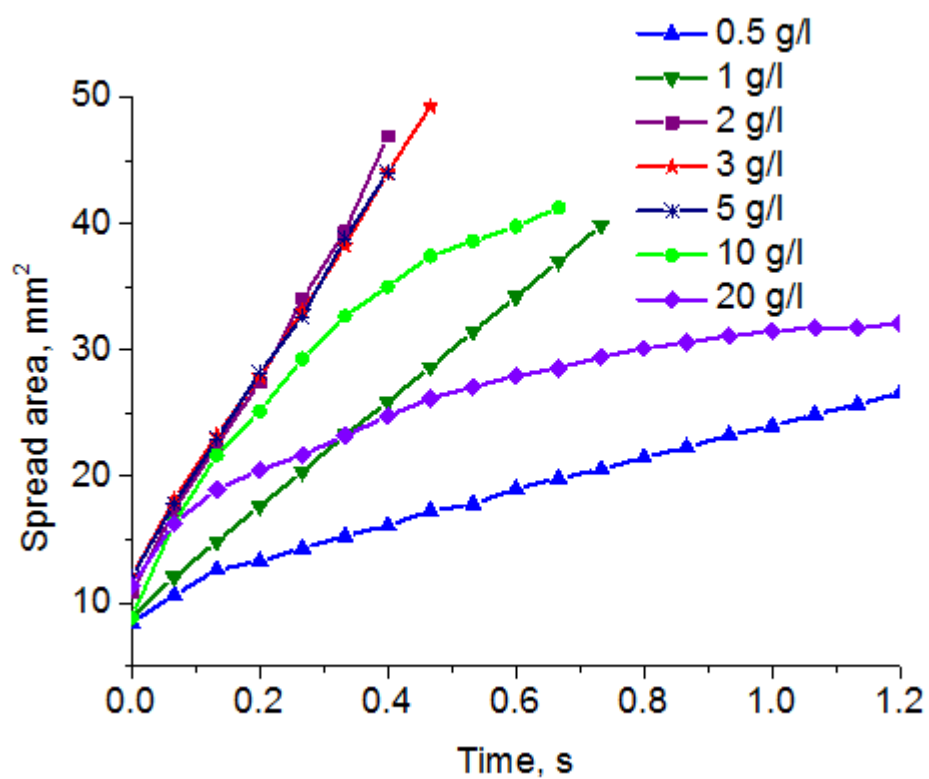
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Graphical abstract



Highlights:

- spreading of mixed solutions of cationic and anionic surfactants
- synergetic effect of these solutions
- wetting of hydrophobic substrates nearly as superspreader
- spreading rate of mixed solutions is smaller than that of superspreader

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6 **Mixtures of cationic surfactants can be superspreaders: comparison**
7 **with trisiloxane superspreader.**
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19 **Abstract**
20

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22 highly hydrophobic substrate such as polyethylene is investigated. It is shown that
23 due to synergetic effect these solutions can wet hydrophobic substrates nearly as
24 effective as solutions of trisiloxane superspreader BT-278. The spreading factor
25 reaches 70 % of that of superspreader for the most effective mixed solution. At room
26 humidity (40 %) spread area has a maximum vs concentration. However, the
27 maximum was not observed at higher humidity 80 %. The spreading rate of mixed
28 solutions is smaller than that of superspreader despite the same spreading exponent
29 $\alpha=0.5$.
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42 Keywords: sodium alkane sulfonates, interfacial tension, spreading kinetics,
43 spreading factor, polyethylene substrate.
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Introduction

Improvement of wettability of hydrophobic substrates by aqueous formulations is of great importance for various industries such as oil recovery; printing, painting and coating; treatment of plants and soils with pesticides, herbicides and fertilisers in agriculture; eye lubricants and treatment of respiratory dysfunctions in medicine etc. Water does not wet low energy surfaces because it has a very high surface energy (surface tension ~ 72 mN/m at room temperature) as compared with other liquids except for liquid metals. Surfactants lower both liquid/vapour and solid/liquid interfacial tensions and in this way facilitate wetting. Trisiloxane surfactants are the most effective known wetting agents frequently referred to as superspreaders. Trisiloxanes promote complete wetting by aqueous solutions of hydrophobic substrates, on which pure water has contact angle around 100° and higher (polyethylene, polypropylene, parafilm) [1, 2]. Aqueous trisiloxane solution can cover area up to 100 times larger than that covered by pure water and spreading process occurs relatively fast on the time scale of tens of seconds.

The most famous trisiloxane superspreader has a structure presented in Fig. 1 and is known under trade names Silwet-L77 and BREAK-THRU S 278; some other abbreviations, including those related to the structure, are also used in literature (see [1, 2] for examples).

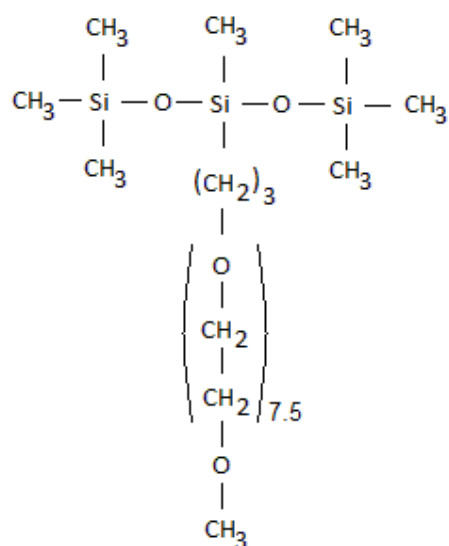


Fig. 1. The structure of trisiloxane surfactant known under the trade names Silwet-L77 and BREAK-THRU S 278.

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6 Ability of trisiloxane surfactants to wet completely hydrophobic substrates is related
7 to their very low surface tension, 20-22 mN/m [3-5] and good adsorption on
8 hydrocarbon surfaces: according to [3] interfacial tension between aqueous
9 trisiloxane solutions and tetradecane is close to zero.

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14 However, the very high rate of spreading of trisiloxane solutions is much less
15 understood. In the case of pure liquids complete spreading is driven by interplay of
16 capillary forces, disjoining pressure and viscous resistance in the vicinity of the
17 three-phase contact line [6]. The latter results in well-known Tanner law [6, 7], with
18 $\alpha=0.1$:
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$$22 \quad R(t) = At^\alpha \quad (1)$$

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26 or

$$27 \quad S(t) = A_1 t^{2\alpha} \quad (1a)$$

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32 where $A = K \left(\frac{V^3 \sigma_{lv}}{\mu} \right)^\alpha$, $A_1 = A^2$, $R(t)$ is the radius of base of a spreading droplet, $S(t)$
33 is its area, K and K_1 are the numerical (dimensionless) coefficients depending (rather
34 weakly [6]) on parameters of disjoining pressure isotherm (Hamaker constant), V is
35 the droplet volume, σ_{lv} is the liquid/vapour surface tension, μ is the dynamic viscosity
36 of the liquid and t is time.
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43 Assuming the same mechanism of spreading, one can expect that surfactant
44 solutions should spread with the same rate or even slower than pure liquids in the
45 case of complete wetting, because at spreading of surfactant solutions two extra
46 relaxation processes are added: adsorption of surfactant molecules at liquid/vapour
47 and solid/liquid interfaces. It was proven in [8] that a very slow spreading kinetics of
48 solutions of fluoro-surfactant Novec FC-4430 is directly related to its slow adsorption
49 kinetics.
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56 However, comparison of spreading kinetics of solutions of trisiloxane surfactants and
57 pure liquids show a substantial difference in favour of the surfactant solutions (Fig. 2),
58 with $\alpha=0.1$ for silicone oil and $\alpha=0.5$ for aqueous solution of trisiloxane surfactant.
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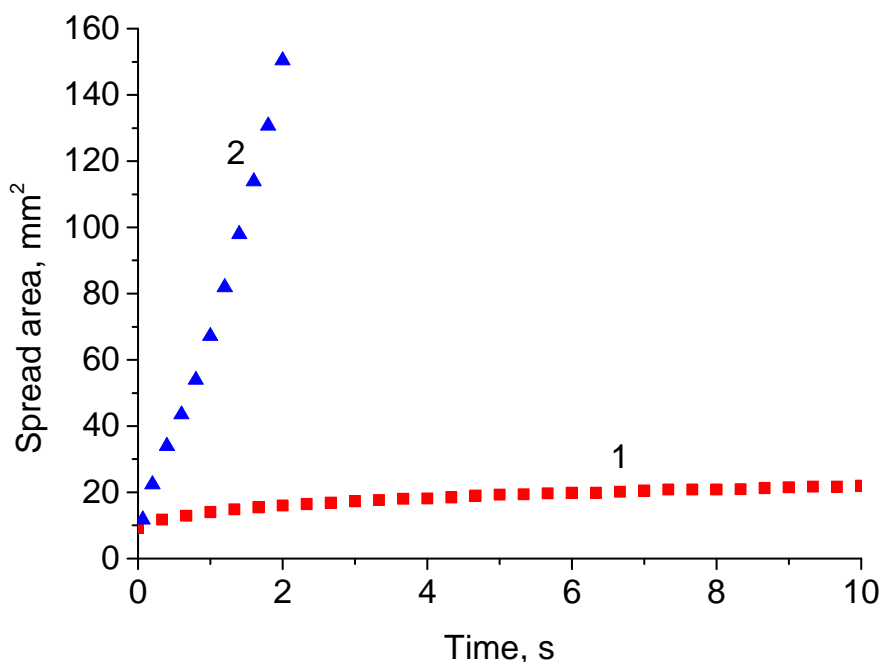


Fig. 2. Spreading kinetics of silicone oil (1) and 1 g/l aqueous solution of trisiloxane surfactant BREAK-THRU S 278 (2) on polyethylene substrate.

Spreading kinetics $R(t) \sim t^{0.5}$ is a characteristic feature of diffusion governed processes. Exactly this power law kinetics was found for spreading of pure trisiloxane surfactant (without water added) [9], however, the spreading was very slow, with spreading rate in the range from mm^2/day to mm^2/hour depending on humidity. An increase in humidity from 30 to 100 % resulted in the 10 times increase of apparent diffusion coefficient. Therefore interaction with water is essential for understanding the fast spreading mechanism.

It is well known [10] that the main energy in the course of spreading is burned in a vicinity of three phase contact line (inside thin precursor film in front of the apparent three phase contact line). The fast spreading of superspreaders suggests that it proceeds according to a different mechanism: cannot be thin precursor films in front of the moving apparent three phase contact line in the case of spreading over hydrophobic substrates. It was the reason why a caterpillar motion in the vicinity of the three phase contact line has been suggested as an explanation of the

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4 superspreading phenomenon [11]. The caterpillar motion in the case of advancing
5 three phase contact line has been suggested earlier in [12] based on the s-shape of
6 disjoining pressure isotherm of aqueous solutions. The disjoining pressure
7 isotherm of trisiloxane solutions is still unknown, that is, the caterpillar motion in the
8 case of superspreading is to be confirmed.
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13 However, there is a possibility that Marangoni flow [13] is also an essential
14 contribution to the superspreading phenomenon.
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17 To elucidate the precise mechanism and predict spreading performance based on
18 the known surfactant properties, additional investigations are required, in particularly
19 those comparing spreading of various surfactants.
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23 It should be emphasised that the spreading performance depends essentially on the
24 experimental conditions such as ambient humidity, substrate roughness and even
25 the protocol of the solution preparation [14, 15]. For example, according to [15]
26 sonicated solution of trisiloxane surfactant spread about 2.5 times faster than the
27 hand shaken one. That is why it is extremely important to perform comparative
28 studies using identical substrates, identical ambient conditions and identical
29 experimental protocols. Results of such comparative study are presented below.
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33 It is well known that solutions of other (non-trisiloxane) surfactants, both non-ionic
34 (oxiethylated alcohols) [16] and ionic (sodium bis(2-ethylhexyl) sulfosuccinate, AOT,
35 and didodecyldimethylammonium bromide) [17] demonstrate a fast spreading with
36 $S \sim t$, but on partially wetted substrates characterised by the contact angle of pure
37 water $\sim 50-70^\circ$. It is suggested below to use the synergism in the performance of
38 surfactant mixtures [18] to get the superspreading on highly hydrophobic substrates
39 such as polyethylene without trisiloxane superspreaders. Promising candidates for
40 this are mixtures of cationic and anionic surfactants, catanionic mixtures [19, 20].
41 Below the wetting performance of series of catanionic mixtures related to their
42 surface properties is analysed, and compared with solutions of trisiloxane
43 superspreader (Fig. 1).
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Experimental

Dodecyltrimethylammonium bromide, DoTAB, (Fluka, 99%); sodium 1-decanesulfonate, SDeS, (Fluka, 99%); sodium 1-octanesulfonate monohydrate, SOcS, (Fluka, 99%); sodium 1-heptanesulfonate monohydrate, SHepS, (Fluka, 99%); sodium 1-hexanesulfonate monohydrate, SHexS, (Fluka, 99%); BREAK-THRU S 278, BT-278, (gift from Evonik); silicone oil, Brookfield viscosity standard; heptane (HCROMASOLV®, Sigma-Aldrich, 99%); iso-propanol (Fisher Scientific, analytical reagent grade) have been used without any additional purification. All solutions have been prepared in ultra-pure water produced by Millipore Q (15 MΩ cm).

Low density polyethylene film, PE (GoodFellow), thickness 0.05 mm, has been cut into pieces 4 × 4 cm, washed for 15 min with iso-propanol in ultrasonic bath, rinsed with plenty of water and dried in an oven at 50 °C. The film roughness measured by AFM is $R_{\text{rms}} = 34.5 \pm 1.2$ nm at scan size 80 μm [20]. The film was placed on the microscopic glass slide support ($R_{\text{rms}}=1.9\pm 0.2$ nm). Contact angle of water on this combined substrate was $101 \pm 3^\circ$.

Contact angle and interfacial tension have been measured with DSA-100 (Kruss) using bubble/drop shape analysis. It is impossible to measure directly liquid/solid interfacial tension. It was the reason why water/heptane interface was used as a representative model. To prevent depletion of aqueous solutions due to partition into the oil phase the corresponding interfacial tension was measured using heptane droplet placed into aqueous solution with v:v ratio about 1000. Consequent measurements on the series of droplets (up to 10) have shown the same value of equilibrium interfacial tension proving that depletion due to partition can be neglected.

All spreading experiments have been performed at room temperature $T=23\pm 1^\circ\text{C}$ and relative humidity $\text{RH}=40\pm 5$ if not otherwise stated. Kinetics of spreading was measured using the series of the images of spreading droplets (top view) taken by video camera at 15 fps. The areas have been calculated using ImageJ free software. The spreading factor was calculated as a ratio of maximum spread area and the area covered by a droplet of pure water of the same volume, 14 μl. The long-time kinetics was measured using 14 μl droplets, whereas the short-time kinetics was measured using 2 μl droplets.

Results and discussion

Equilibrium contact angle of a liquid droplet on a solid substrate is determined by the energy balance given by the Young equation:

$$\cos\theta = \frac{\sigma_{sv} - \sigma_{sl}}{\sigma_{lv}}, \quad (2)$$

where σ_{sv} , σ_{sl} , and σ_{lv} are the solid/vapour, solid/liquid and liquid/vapour interfacial tensions. As experimentally measurable quantities are advancing and receding contact angles, the best approximation for θ is considered to be static advancing contact angle [22]. Complete wetting occurs when the right hand side of Eq. (2) becomes positive, i.e.:

$$\sigma_{sv} - (\sigma_{sl} + \sigma_{lv}) > 0 \quad (3)$$

and contact angle does not exist anymore ($\cos\theta > 1$). Inequality (3) means that it is energetically favourable to replace the solid/vapour interface by two other interfaces: solid/liquid and liquid/vapour. Eq. (3) shows that a decrease of solid/liquid and liquid/vapour surface tension favours wettability of the solid surface.

Minimum attainable interfacial tension at water/air and water/alcane interfaces due to adsorption of individual ionic surfactants used is essentially higher than that of trisiloxane solutions: DoTAB enables lowering the water/air surface tension to ~38 mN/m and water/alcane interfacial tension to ~5 mN/m [22]. Very close value of water/air surface tension was found below for SOcS, whereas water/heptane interfacial tension was even higher than that of DoTAB: ~10 mN/m (Fig. 3).

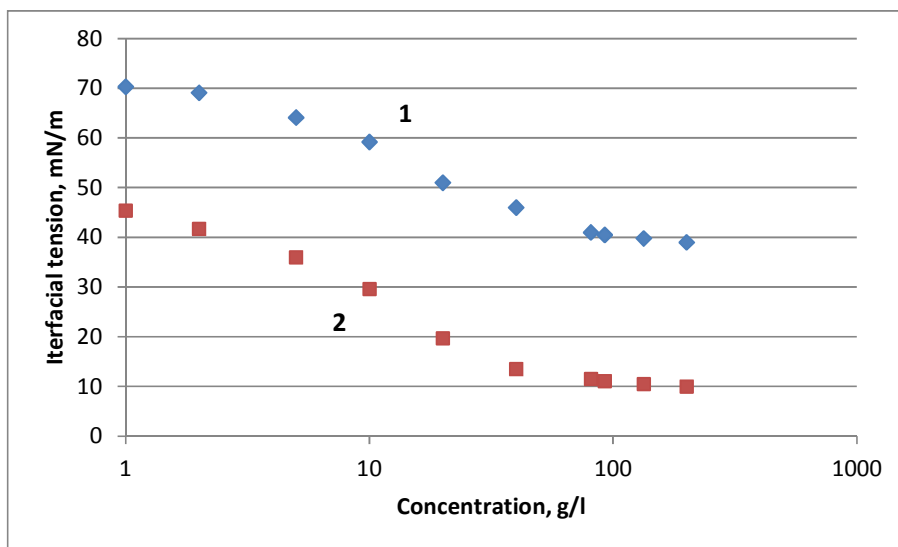


Fig. 3. Interfacial tension isotherms of SOcS: 1 – at water/air interface, 2 – at water/heptane interface. For this surfactant cmc ~100 g/l and it does not wet completely polyethylene (CA~66°) (see below).

Comparison of values of minimum attainable interfacial tensions (Fig. 3) with the data for the trisiloxane superspreaders (20-22 mN/m at water/air [3-5] and close to zero at water/alkane [3] interface) shows that they are considerably higher than corresponding values found for trisiloxanes. The comparison shows that solutions of individual ionic surfactants under investigation should spread worse than those of trisiloxane surfactants. Indeed individual ionic surfactants used demonstrated only partial wetting on the polyethylene substrate with contact angle in the range of $66.5 \pm 1^\circ$ for solutions of SOcS at concentrations above cmc (~100 g/l).

When cationic and anionic surfactants are mixed together then electrostatic repulsion between individual ionic surfactant molecules is replaced by electrostatic attraction between oppositely charged parts of molecules. This results in closer packing of molecules in adsorption layers and, consequently, lower interfacial tension on both water/air and water/alkane interface as can be seen in Figs. 4 and 5.

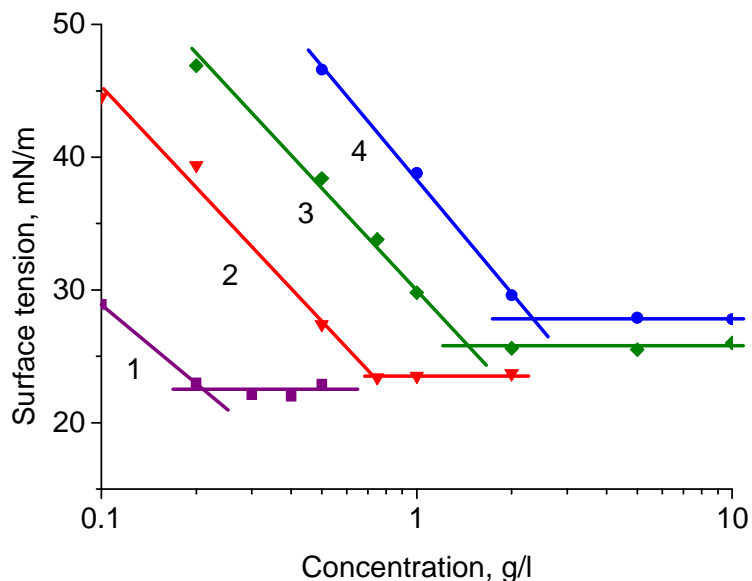


Fig. 4. Equilibrium interfacial tension at water/air interface for v:v=1:1 mixture of DoTAB with: 1 – SDeS, 2 – SOcS, 3 – SHepS, 4 – ShexS.

Cmc can be found from Fig. 4 as the intersection points of two straight lines. It should be noted that for trisiloxane surfactants superspreading begins at concentration called critical wetting concentration (cwc) which is several times higher than their critical aggregation concentration (cac). Cwc for cationic mixtures can be found from Fig. 6, but for these mixtures difference between cmc and cwc is inside the experimental error, i.e. there is no essential difference. At concentrations above cmc the water/heptane interfacial tension was very low: it was impossible to measure interfacial tensions below 1.5 mN/m using drop shape analysis, because spontaneous emulsification occurred preventing the drop formation.

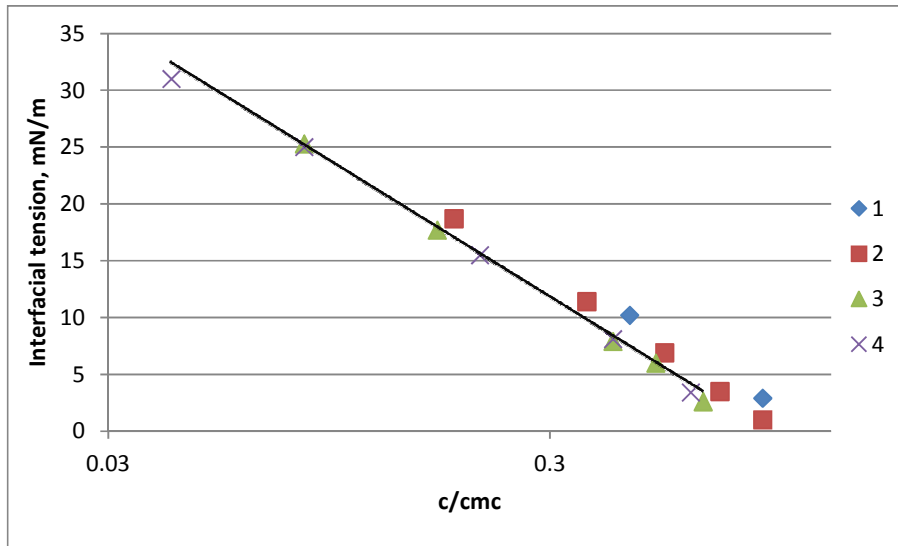


Fig. 5. Equilibrium interfacial tension at water/heptane interface for v:v=1:1 mixture of DoTab with: 1 – SDeS, 2 – SOcS, 3 – SHepS, 4 – SHexS. Cmc values are the same as in Fig. 4.

Water/air interfacial tension increased with the decrease of chain length of sodium alkane sulfonate. The low values of water/air interfacial tension, which are comparable with that for BT-278, enabled complete wetting for all mixtures except SHepS. For mixture DoTAB with SHexS only partial wetting occurred with contact angle about 13° at concentrations above cmc.

In cationic mixtures both micellisation and the macroscopic phase separation can take place. For the mixture SDeS+DoTAB the latter resulted in crystallization with the limit of solubility being lower than cmc (see [20] for details and its effect on the spreading performance). For the mixture SOcS+DoTAB the liquid phase separation becomes clearly visible at concentration 5 g/l, with milky phase creaming on the top of the clear solution. In this case phase separation occurs at concentration above cmc.

Comparison of spreading factors for superspreader BT-278 and cationic mixtures is given in Fig. 6. The spreading factor decreases with the decrease of the chain length from SOcS to SHexS due to increase of water/air surface tension: SDeS is C12, SDeS is C10, SOcS is C8, SHepS is C7 and SHexS is C6.

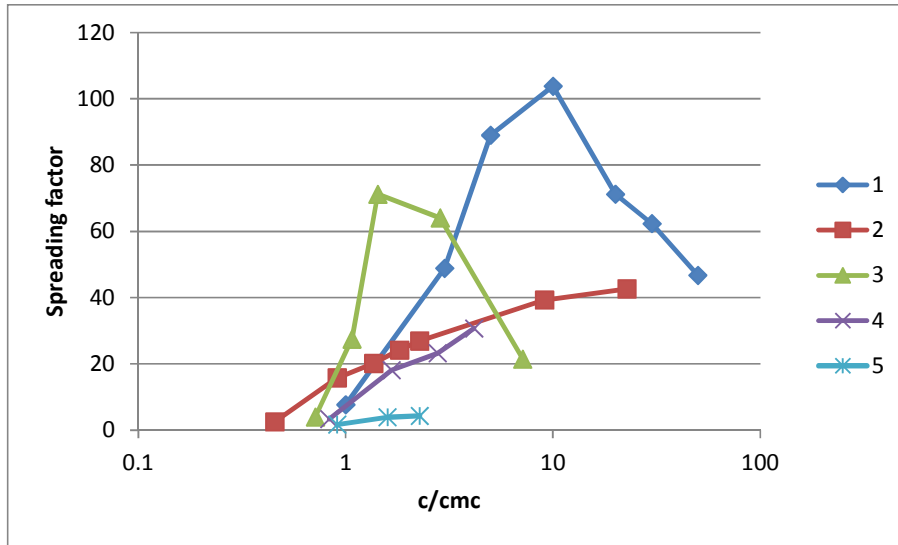


Fig. 6. Spreading factors calculated for 14 μ l droplet of 1 – BT-278 and v:v=1:1 mixture of DoTAB with: 2 – SDeS, 3 – SOcS, 4 – SHepS, 5 – SHexS.

In experiments performed at ambient humidity the spread area reached a maximum at certain concentration of solution and then decreased. It is interesting that the maximum of the spread area for BT-278 and the mixture of DoTAB with SOcS are observed at the identical concentration 1 g/l. The maximum in the spread area of trisiloxane surfactant at concentration 1 g/l agrees with the results presented in [23] for Silvet L-77, which is similar to BT-278.

Note, at concentrations above those presented in Fig. 6 there is a transition from complete to partial wetting even for the superspreader. For example, the solution of BT-278 with concentration 100 g/l (which is above both $cac/cwc \sim 1000$ cac or 400 cwc) had the contact angle on PE around 20°. After some time, this sessile droplet of this solution shrunk due to evaporation leaving an area covered by trisiloxane only; surprisingly this remaining area is not wetted by more diluted solutions of BT-278: droplet of solution of 1 g/l (which is 10 cac or 4 cwc), which demonstrated the best wetting properties on polyethylene, spread around this area and avoided the deposit, which remained after evaporation of 100 g/l solution. That means the deposit was much more hydrophobic than polyethylene itself.

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4 The picture changes considerably at higher humidity. In this case the spread area
5 increased with concentration in the whole studied concentration range. At RH=40 %
6 the spread area of BT-278 at concentration 10 g/l (100 cac) was about 5 times
7 smaller than that at concentration 1 g/l (10 cac). At RH=80 % spread area increased
8 for both concentration, but only doubled for 1 g/l (10 cac), whereas more than 10
9 times increase was detected for 10 g/l (100 cac), i.e. at this high humidity spread
10 area of 10 g/l (100 cac) solution was about 1.5 times larger than that of 1 g/l (10 cac)
11 solution. Considerably larger increase in the spread area for more concentrated
12 solutions shows that the increase in the spread area caused by the increase of
13 humidity was the result not only of the slower evaporation, but it was related to the
14 change in the spreading properties of solution itself: the thickness of spread film in
15 the end of the spreading process of 10 g/l (100 cac) solution of BT-278 was about 20
16 μm at RH=40 % and it decreased to 1-2 μm at RH=80 %. Spreading time was of
17 order of 10 s for both concentrations at RH=40 %, after that time the spread area
18 began to decrease because of evaporation for 1 g/l (10 cac) solution. For
19 concentration 10 g/l (100 cac) evaporation occurred much slower because of much
20 smaller radius of the spread film: liquid evaporated completely within 10-15 min. At
21 RH=80 % spreading time of 1 g/l (10 cac) solution remained the same around 10 s,
22 but 10 g/l (100 cac) solution spread over 10 min. It is interesting that if a substrate
23 with a spread at RH=40 % droplet of BT-278 at concentration of 10 g/l (100 cac) was
24 moved to the chamber with higher humidity (80%) it started to spread further with
25 spread area increasing 8-10 times during around 10 min.

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33 For the mixture SOcS with DoTAB the total spreading time was about 2 min
34 independently of humidity. In this case it looks like the spreading stopped, because
35 dewetting came into play. Nevertheless, similarly to BT-278 the spread area
36 increased with the increase of humidity and the increase was more pronounced at
37 higher concentrations: spread area increased by about 50 % for concentration 1 g/l
38 (1.4 cmc) and 4-5 times for concentration 10 g/l (14 cmc) at the increase of humidity
39 from 40 % to 80 %. The scattering in the results was very high in this case and the
40 difference in the spread area for 1 g/l (1.4 cmc) and 10 g/l (14 cmc) at RH=80 % is in
41 the range of experimental error with average being a little bit higher for 10 g/l (14
42 cmc).

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4 During spreading of BT-278 a circular shape retained all the time with the small
5 fingers appearing before the end of the spreading. The shape of spread of cationic
6 mixture solution was less regular. After the maximum area had been reached, the
7 dewetting was observed for all cationic solutions: the spread film retreated
8 reassembling back in the droplet. The reassembling process was more pronounced
9 at higher concentrations. This phenomenon was already described earlier for the
10 mixture of SDeS with DoTab [20]. In that case the reassembled drop had a large
11 contact angle (about 50°) and the phenomenon was related to the increase of
12 surface tension due to crystallisation. The crystallization did not occur in mixed
13 solutions of DoTAB with sodium alkane sulphonates with hydrophobic chain length 8
14 and less than 8 hydrocarbon groups. Liquid/liquid phase separation was observed
15 for SOcS at concentrations 5 g/l (67 cmc) and above. Mixed solutions with SHepS
16 remained clear till concentration 10 g/l (6 cmc). Nevertheless the dewetting was
17 observed even in this case. Note, in two last cases contact angle remained very small
18 after dewetting.
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30 Short time spreading kinetics of solution BT-278 is presented in Fig. 7 and that of the
31 most effective cationic mixture SOcS+DoTAB in Fig. 8. Note, the inertial or
32 viscous stages of spreading, which develop on shorter time scale [24,25] were not
33 considered: only kinetics of spreading on the time scale from hundred milliseconds to
34 seconds was investigated, i.e. during the superspreading stage [24]. Experimental
35 errors at measurements of spreading kinetics at the early stage were smaller for BT-
36 278 (not exceed $\pm 10\%$) than for cationic mixture ($\pm 20\%$). Kinetics virtually did not
37 change at the change in humidity: difference in kinetics between RH=40 % and
38 RH=80 % was in the range of experimental error.
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47 Figs. 7 and 8 show that at concentrations below 10 g/l (100 cac) for BT-278 and
48 below 5 g/l (6.7 cmc) for the mixture SOcS+DoTAB spread area increased linearly
49 with time over the studied time interval, but at larger concentrations spreading
50 slowed down after the linear part. The same slowing down was found for other
51 concentrations as well, but occurred at larger times as it is presented in Fig. 9, where
52 the long-time kinetics is presented for some selected solutions. For BT-278, 10 g/l
53 (100 cac) the linear stage is absent in Fig. 10, because it ended much earlier as it is
54 shown in Fig. 7. This slowing down is the reason why spread area demonstrates a
55 maximum vs concentration at 40 % humidity.
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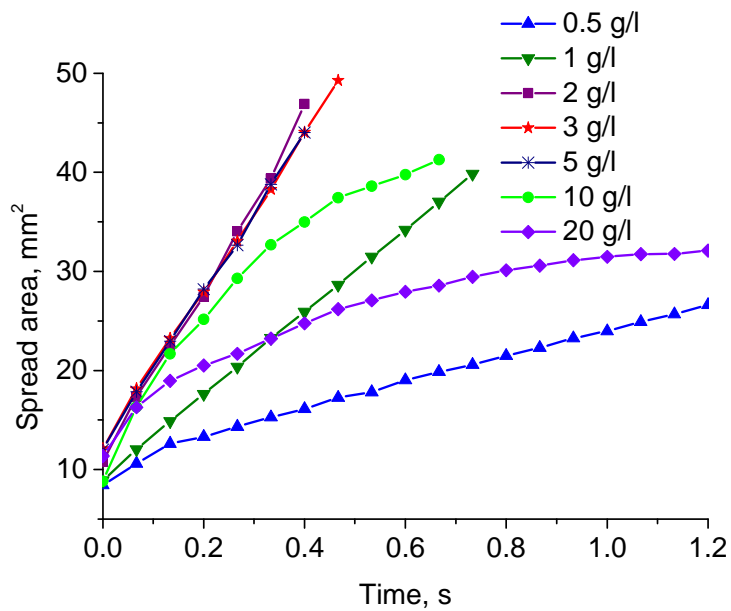


Fig. 7. Kinetics of spreading of BT-278 trisiloxane superspreader at various concentrations. Droplet volume 2 μ l.

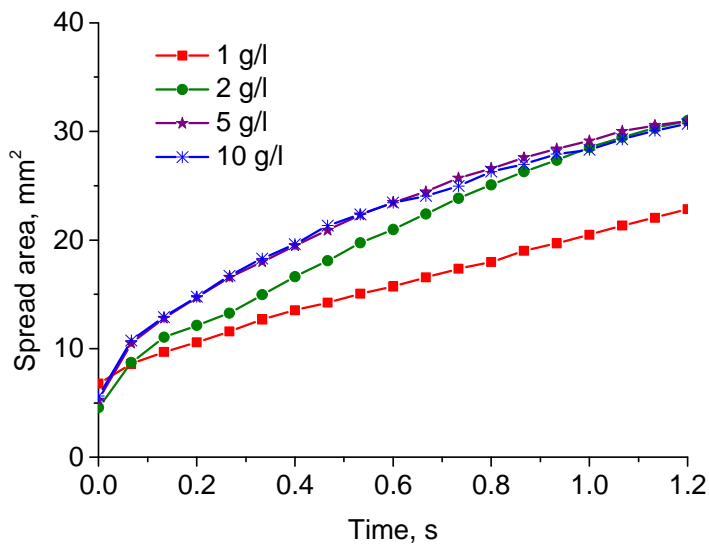


Fig. 8. Kinetics of spreading of mixture SOcS+DoTAB at various concentrations. Droplet volume 2 μl .

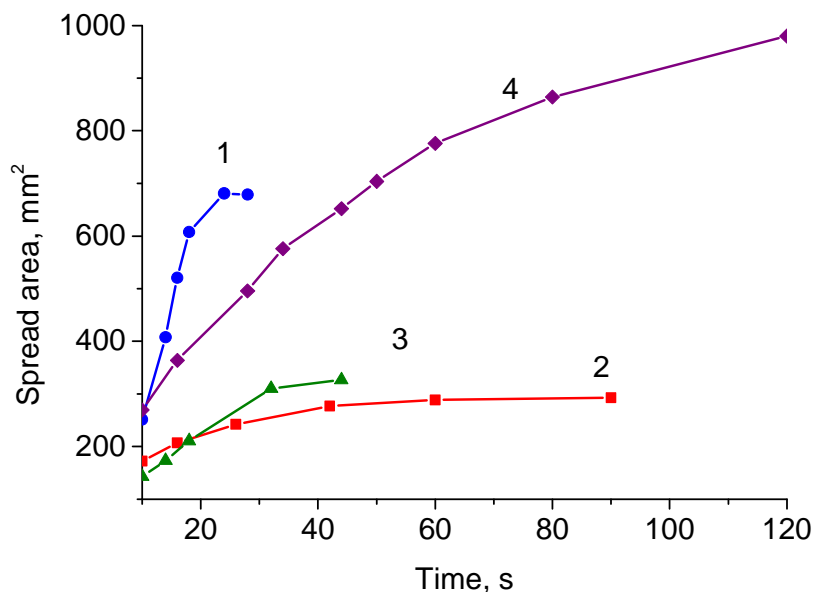
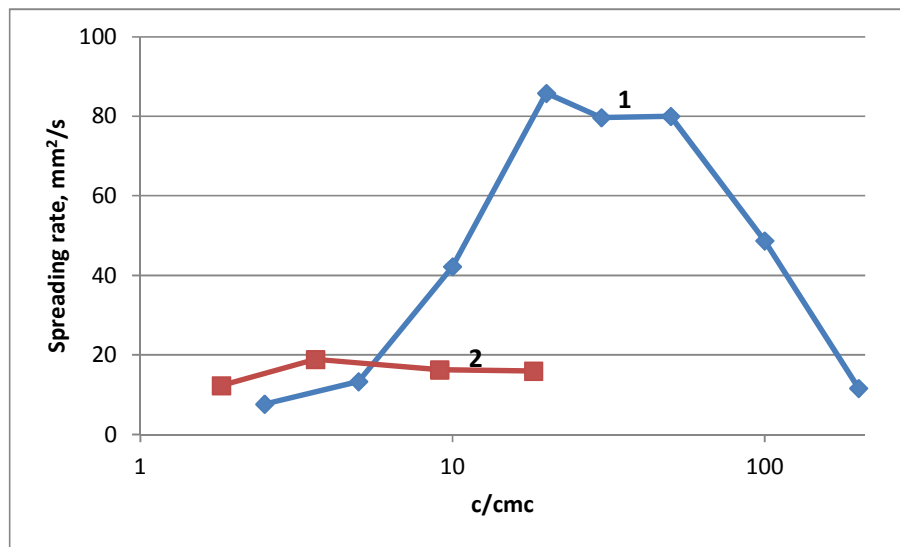


Fig. 9. Long time kinetics of spreading: 1 – BT-278, 0.3 g/l; 2 – BT-278, 10 g/l; 3 – SHepS+ DoTAB, 10 g/l, 4 – SOcS+DoTAB 1 g/l. Droplet volume 14 μl .

Concentration dependences of the short time spreading rate for BT-278 and mixture SOcS+DoTAB are summarised in Fig. 10. The values shown in Fig. 10 are the averaged values during the first recorded second of spreading. The essential decrease in the spreading rate of BT-278 at concentrations 10 and 20 g/l are the result of the early slowing down of the spreading. If we consider the spreading rate as an initial slope of curves in Figs. 8 and 9 then it can be concluded that it increases and reaches plateau at concentrations above 2 g/l for both surfactants (see Figs. 7 and 8).

Note, the spreading rate for the mixture SOcS+DoTAB is nearly 5 times lower than that for BT-278 despite the same spreading exponent $\alpha=0.5$. That is, factor A_1 in Eq. (1a) is much larger for solutions BT-278 as compared with catanionic mixtures. The mechanism of spreading and the big large difference in factor A_1 for different

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4 surfactants is to be explained. Note, the case of the spreading of pure liquids A_1
5 does not vary considerably [6]. For example, the difference in A_1 at spreading of
6 silicone oil over PE (contact angle of water 101°) and clean glass(contact angle of
7 water close to 0) is only about 12 % despite the large difference in the energy of
8 substrates.
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38 Fig. 10.Short time spreading rate vs concentration for 1 – BT-278 and 2 – mixture of
39 DoTAB+SOcS solutions.
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45 Conclusions

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47 Mixtures of dodecyltrimethylammonium bromide with sodium alkane sulfonates C6-
48 C10 demonstrated essential synergism in surface activities and in wetting
49 performance. The best wetting inside v:v=1:1 mixtures was achieved with
50 DoTAB+SOcS at concentration 1 g/l (~1.4cmc). Comparative study performed at the
51 same conditions has shown that spreading factor of this mixture reaches about 70 %
52 of spreading factor of trisiloxane superspreader BREAK-THRU S 278.
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58 Spreading rate of cationic mixtures is considerably lower as compared with BT-
59 278: the maximum spreading rate of DoTAB+SOcS mixture is nearly 5 times smaller
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4 than that of BT-278. At the same time spreading of mixtures lasts longer, resulting in
5 comparable with BT-278 spread areas.
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8 Initial rate of spreading increased with surfactant concentration until the maximum
9 was reached for all surfactants solutions and in the range of concentrations studied,
10 and then initial rate of spreading started to decrease slowly. At the same time the
11 spread area went via maximum value. The spread area is determined by both
12 spreading rate and the time of spreading. It was found that the spreading process
13 started to slow down earlier at higher concentrations.
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19 An increase in humidity resulted in an increase of spreading time and consequently
20 in the increase of the spread area. The increase in the spread area caused by the
21 increase of humidity was not only result of slower evaporation rate, but it was also
22 related to the change in the spreading properties of the solution itself.
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