



Dodecahedral W@WC Composite as Efficient Catalyst for Hydrogen Evolution and Nitrobenzene Reduction Reactions

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Supporting Information

ABSTRACT: Core-shell composites with strong phase-phase contact could provide an incentive for catalytic activity. A simple, yet efficient, H_2O -mediated method has been developed to synthesize a mesoscopic core-shell W@WC architecture with a dodecahedral microstructure, via a one-pot reaction. The H_2O plays an important role in the resistance of carbon diffusion, resulting in the formation of the W core and Wterminated WC shell. Density functional theory (DFT) calculations reveal that adding W as core reduced the oxygen adsorption energy and provided the W-terminated WC surface. The W@WC exhibits significant electrocatalytic activities toward hydrogen evolution and nitrobenzene electroreduction reactions, which are comparable to those found for commercial Pt/C, and substantially higher than those found for meso- and nano-WC materials. The experimental results were explained by DFT calculations based on the energy profiles in the hydrogen evolution reactions over WC, W@WC, and Pt model surfaces. The W@WC also shows a high thermal stability and thus may serve as a



promising more economical alternative to Pt catalysts in these important energy conversion and environmental protection applications. The current approach can also be extended or adapted to various metals and carbides, allowing for the design and fabrication of a wide range of catalytic and other multifunctional composites.

KEYWORDS: tungsten, tungsten carbide, core-shell structure, self-assembly, electrocatalyst, density functional theory, hydrogen evolution

1. INTRODUCTION

Composite materials are fundamentally important in both academic studies and industrial applications. Incorporation of bi- or tri-component materials can improve insufficient activity possessed by single component materials. Studies have shown that the surface structure of a composite has a strong influence on its stability and catalytic properties.¹⁻³ Transition metal carbides such as WC, TiC, and MoC and their composites are becoming increasing important due to their diverse physical and chemical properties for various applications.^{4–9} WC materials, in particular, have demonstrated platinum-like surface properties in many surface science and catalysis studies, including those initially investigated by Levy and Boudart¹⁰ and more recently by Bosco.¹¹

To date, many investigations have paid attention on increasing the specific surface area of WC to improve the (electro)-catalytic activity. However, WC (or WC/C composites) materials with high surface area still show a low activity.¹¹ Our previous research has focused on the catalytic improve-

ment of WC single-phase materials and WC composites.^{3,12–14} Nanosized and mesoporous WC materials were prepared which did exhibt improved electrocatalytic activity; nevertheless, they are still incomparable with the commercial Pt catalysts. The main difficulty for improving activity seems to be due to the fact that carburization requires a high temperature which reduces the possibility of controlling the surface structure. Chen and his group have shown that tungsten carbides are a class of materials very challenging to work on due to complications related to carbon, oxides and defects being present on surface, as well as phase purity and surface termination.^{15–17} Surface reactivity toward chemisorption and catalysis are often inhibited by polymeric carbon deposited on carbide surfaces during the carburization processes.¹⁸ It was believed that the most active WC was slightly carbon deficient in the carbon layers of the

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WC lattice.¹⁹ However, the challenges of synthesizing and maintaining a clean (free from deposited carbon and with W-terminated) and stable WC surface still need to be overcome.

Typically, the W precursor (ammonium tungstate) was carburized to form WC at 850 °C. Although the WC surface exhibits as normal WC planes, some C vacancies would be inevitably replaced by O atoms.^{20,21} These in turn would resist the exposure of the W-terminated surface. During the catalytic reaction, the O atoms should be removed to reactivate the Wterminated WC surface layer. Following the progress of our understanding, we are interested in developing the WC composite with strong phase-phase bonding to further improve the catalytic activity through exposing the Wterminated WC surface layer. Engineering a composite having a multilayer structure with WC as the surface layer and carbonfree materials as the bottom layer is considered as an effective way to balance these surface properties for resisting the trend of carbon atoms being transported outward. We expect that the core-shell W@WC structure with mixed W-terminated WC shell is a promising candidate, as using W as the core can combine favorable properties of a core-shell structure,^{22,23} as well as reduce the surface O adsorption energy.

In this work, we propose and demonstrate a simple, yet novel, method to synthesize W@WC bilayer particles with a primary W-terminated WC top layer. H_2O , serving as a clean "catalyst", mediated the direction of crystal growth. This is a one-pot and scalable synthsis method and is capable to be adapted to produce multifuctional WC based materials in large-scale.

2. EXPERIMENTAL AND MODELING SECTION

2.1. Synthesis of W@WC. Ammonium metatungstate (AMT, $(NH4)_2W_4O_{13}$ ·xH₂O) was dissolved in deionized water with a weight percentage of 10% and then treated by spray-drying (BÜCHI Spray Dryer B-290) to produce hollow spheres. The precursor was prepared in a corundum boat and dried in a tube furnace under flowing nitrogen gas for 1 h. This sample underwent the gas–solid reaction under an atmosphere of CO/CO₂/H₂O. The schematic diagram of the setup used for the synthesis of W@WC is shown in the SI (Figure S2). The flow rates of CO and CO₂ gases were 300 and 30 cm³ min⁻¹, respectively. Initially, furnace temperature was raised to 400 °C and maintained for 2 h after the reaction zone was free from oxygen. The water was introduced by vaporizing deionized water to wet the airflow at the entrance of the reaction zone. Thereafter, the temperature was raised to 850 °C and maintained for 12 h. The sample was cooled to 0 °C at the end of the reaction.

2.2. Characterization. The phases present in the synthesized material were identified using XRD (Panalytical X'Pert Pro) and TGA (Seiko Instruments, Pyris Diamond). The morphology and structure of the products were characterized using FE-SEM (Hitachi S-4700 II) and TEM (Tecnai G2 F30) and HR-TEM with EDS. The specific surface areas of the sample pores were measured by a nitrogen adsorption–desorption analyzer (Micromeritics ASAP 2020). The surface compositions of the resultant microparticles were detected by the XPS recorded on a Kratos AXIS Ultra DLD, using a monochromated Al K α X-ray as the excitation source, and the binding energies were corrected using Au $4f_{7/2}$ (84.0 eV) as the reference line.

2.3. Electrochemical Measurements. The electrocatalytic properties of the W@WC were analyzed by employing the powder microelectrode (PME, 60 μ m in diameter) approach. The structure and preparation of the PME have been described previously.²⁴ The WC samples were ground and inserted into the lower tip of the electrode.²⁵ Cyclic voltammetry of W@WC was carried out using an electrochemical station (CHI-660c), where reduction current is defined as positive current.

2.4. DFT Calculation Method. All the electronic structure calculations were performed using the Vienna Ab-initio Simulation Package (VASP) with the exchange-correlation functional of Perdew-Burke-Ernzerhof (PBE). The projector-augmented wave (PAW) pseudopotentials were utilized to describe the core electron interaction. Geometry optimization was carried out by the BFGS algorithm. $^{26-33}$ The cutoff energy was 400 eV, and a 4 × 4 × 1 Monkhorst-Pack k-point sampling was used. Four layers of the Wterminated WC(0001) surface was used in the calculation. For modeling the W@WC materials, the $p(3\times3)$ W(110) surface was used as the core structure and C atoms were set up in the first and second subsurface, keeping the ratio of W:C equal to 1:1. We modeled $W(110)@WC_{1L}$ [one layer of WC on W(110)] and $W(110)@WC_{2L}$ [two layers of WC on W(110)] surfaces with different quantities of C atoms to represent the W(@WC materials. The bottom two layers were fixed while the top two layers were allowed to relax during calculations. The vacuum region was ~12 Å to ensure that there is little interaction between slabs. The top and side views of the models are shown in Figure S1. For each adsorbate, different binding sites were calculated to determine the most stable bonding configuration. The adsorption energy was defined as eq 1

$$E_{ad} = E(adsorbate/surface) - E(adsorbate) - E(surface)$$
(1)

where E(adsorbate/surface), E(adsorbate), and E(surface) are the total energies of the adsorbate binding with the surface, gaseous adsorbate, and clean surface, respectively. The Gibbs free energy can be written as G = E + ZPE - TS, where ZPE is the zero point energy, S is the entropy, and T is the temperature of 298.15 K.

2.5. DFT Calculations of Catalytic Activity toward Hydrogen Evolution Reaction (HER). Norskov's group have provided a theoretical model to explain the origin of the volcano curve in HER kinetically, which is in good agreement with experiments and has been widely used in the understanding of the catalytic activity in hydrogen evolution reactions.^{34–37} In this general model, the kinetics is determined by the hydrogen adsorption free energy, $\Delta G(H^*)$.

The total hydrogen evolution reaction can be written as

$$2H^+ + 2e^- \to H_2 \tag{2}$$

The reaction 2 is in equilibrium at the condition of standard hydrogen electrode (SHE) (pH = 0, T = 298.15 K), and therefore, the free energy of H⁺ + e–is equal to that of $1/_2$ H₂. The reaction 2 can be decomposed into two steps as reactions 3 and 4. It is noticed that, in this model, the role of the Tafel reaction (2H* \rightarrow H₂) is proved to be limited.

$$\mathrm{H}^{+} + \mathrm{e}^{-} \to \mathrm{H}^{*} \tag{3}$$

$$\mathrm{H}^* + \mathrm{H}^+ + \mathrm{e}^- \to \mathrm{H}_2 \tag{4}$$

Since the reaction barriers are limited by the thermodynamical states, the total reaction rate can be deduced as eq 5

$$r = k_{\rm B}T/h \exp\{-\max(\Delta G_2, \Delta G_3)/RT\}$$
(5)

where ΔG_2 and ΔG_3 are the free energy changes of the following reactions 6 and 7, respectively.

$$\Delta G_2 = G(H^*) - G(H^+ + e^-)$$
(6)

$$\Delta G_3 = G(H_2) - G(H^*) - G(H^+ + e^-)$$
(7)

3. RESULTS AND DISCUSSION

3.1. Theoretical Structural Analysis. The density functional theory (DFT) calculations were performed on oxygen adsorption on W(110)@WC_{1L} (one layer of WC shell), W(110)@WC_{2L} (two layers of WC shell), and WC(0001) surfaces at various oxygen coverages of 0.33, 0.67, and 1 ML, respectively. The relationship between the oxygen adsorption free energy, $\Delta G(O^*)$, and the coverage, $\theta(O^*)$, is shown in Figure 1. Atomic oxygen prefers to occupy the surface hollow



Figure 1. (a) Calculated oxygen adsorption free energy, $\Delta G(O^*)$, at various oxygen coverages, $\theta(O^*) = 0.33$, 0.67, and 1 ML, on W(110)@WC_{1L} (that is one layer of WC shell on top of W core), W(110)@WC_{2L} (that is 2 layers of WC shell on top of W core), and WC(0001) surfaces. (b) Models showing different oxygen coverages on WC(110)@WC and WC(0001) surfaces.



Figure 2. (a-d) SEM images showing the morphologies of (a) the spherical precursor of ammonium metatungstate and (b-d) the dodecahedral W@WC product. (e) TEM image of a nanosized W@WC particle. (f) HRTEM image showing the edge of the dodecahedral particle. (g) Model showing the relationship between the dodecahedral shape and the crystal planes.

site (Figure 1). Oxygen on WC(0001) yields the highest adsorption free energy in the range of -7.53 to -7.70 eV. However, on W(110)@WC_{1L}, the oxygen adsorption free energy is decreased significantly to -7.09 to -7.16 eV, much

lower than those on WC(0001), indicating weaker O adsorption over the composite surface.

Compared to WC, atomic oxygen on W@WC is significantly easier to be reduced/removed with ca. 0.40 V less overpotential

(0.4 eV less in oxygen adsorption energy; see Figures 1 and S1), resulting in more W-terminated sites available for catalytic reactions.

3.2. H₂O-Mediated Synthesis of W@WC. 3.2.1. Material Characterization. The W@WC was synthesized via a one-pot method in a tube furnace (see Figure S2) by carburizing the spray dried precursor (ammonium metatungstate, AMT; see Figure 2a for its morphology). Scanning electron microscopy (SEM) of the W@WC sample revealed the dodecahedral morphology (Figure 2b-d).

The surface of the W@WC is smooth and free of pores. The layered structure of the as-synthesized sample was also observed by powder X-ray diffraction (XRD) analysis (curve 850 $^{\circ}$ C-12 h, Figure 3). The most intense diffraction peaks



Figure 3. XRD patterns and SEM images of the sample at each stage of the reduction-carburization process.

were found at 2θ values of 40.3° and 58.3° , which are consistent with the planes of W(110) and W(200) in JCPDS 04-0806. In addition, there are several additional diffraction peaks with 2θ values of 31.5, 35.7, and 48.4° (Figure 3 and the inset in Figure 4a), which can be assigned to the planes of WC(001), WC(100), and WC(101), respectively, according to JCPDS 25-1047.

To get an insight into the route of the W@WC formation, XRD patterns and SEM images of the sample at each stage of the reduction-carburization process were collected (Figure 3).

Below 400 $^{\circ}$ C, the spherical AMT underwent decomposition and dehydration, forming WO₃ predominantly. Between 400 and 850 $^{\circ}$ C, the sample was reduced in the presence of CO, forming W predominantly.

3.2.2. Synthesis Mechanism. It is noted that CO not only acted as a reductive agent for reducing tungsten oxide but also underwent the following redox reaction (i.e., Boudouard reaction):

$$2CO(g) \to CO_2(g) + C(s) \tag{8}$$

The dynamic ratio of CO/CO_2 in the tube furnace was determined by the Boudouard reaction (eq 8); at temperatures below 700 °C, the predominant products were on the CO_2 (exothermic formation) side, whereas, at higher temperatures, the most dominant product was CO (endothermic formation process). Here, CO_2 was added in the reaction atmosphere to inhibit "Boudouard reaction", and the following water-gas shift reaction became the dominant process at the lower temperatures, which being weakly exothermic (eq 9).³⁸

$$CO(g) + H_2O(g) \rightarrow CO_2(g) + H_2(g)$$
(9)

The presence of H₂O vapor resulted in the production of hydrogen as a secondary reductive agent. During this stage, the macroporous structure of WO₃ was already formed (below 400 °C) on removal of the NH₃ upon decomposition of the NH₄⁺ contained in the AMT. H₂O was also released from the AMT, and it was unlikely to be removed away from the sample as there was abundant H₂O added in the carburization atmosphere. H₂O reacted with WO₃ to form gaseous WO₂(OH)₂ (eq 10; also see Figure S3).³⁹

$$WO_3(s) + H_2O(g) \rightarrow WO_2(OH)_2(g)$$
(10)

 $WO_2(OH)_2$ was then reduced by H_2 to form W in accordance with the eq 11, where W crystallization proceeded as it was being produced.

$$WO_2(OH)_2(g) + 3H_2(g) \rightarrow W(s) + 4H_2O(g)$$
 (11)

According to the Wulff facets theorem,⁴⁰ a crystal formed at equilibrium has to be bound by facets giving a minimum total surface energy. For a body-centered cubic (bcc) crystal structure such as W, the surface energy of the low-index crystallographic facets is given in the order γ {110} < γ {100} < γ {111}.⁴¹ Here, H₂O was added as the catalyst to produce



Figure 4. (a) The XRD patterns of the carburized W@WC sample (1) and the same sample following a second carburization process at 850 °C (2); the inset shows a magnified XRD pattern of the carburized sample. (b) XPS of W 4f features for the W@WC bilayers (black line corresponds to the overall spectrum, and the colored lines indicate curve fitting of the $4f_{7/2}$ and $4f_{5/2}$ spin orbit coupling pairs).

gaseous $WO_2(OH)_2$ as the intermediate (eqs 10 and 11). The absence of crystallization medium in the gas–solid reaction can thus be avoided. On the basis of these factors, the minimum surface-energy requirement predicts that the seed crystals of W should show a tendency to adopt a dodecahedron shape enclosed by {110} facets.⁴² With a high extent of epitaxial growth at high temperature, the aggregates of nanocrystallites form a continuous crystal (Figure 3, SEM images).⁴³ On the other hand, for a comparison, we also used pure and dry H₂ gas directly to reduce the spherical AMT; the yielded particles exhibit a mesoporous structure (Figure S4) rather than the dodecahedral W@WC having the smooth surface.

Due to the loss of volatilizing components (H_2O , NH_3) in the AMT precursor and the instant reduction of $WO_2(OH)_2$, the particle size distribution of the dodecahedral W@WCproduct was largely following the spherical AMT precursor with a little narrowing tendency (Figure S5).

Carburization of the W surface could also take place via the exothermic methane formation as well as via the direct CO reaction to form WC in the following reactions:

$$CO(g) + 3H_2(g) \rightarrow CH_4(g) + H_2O(g)$$
(12)

$$W(s) + 2CO(g) \rightarrow WC(s) + CO_2(g)$$
(13)

$$W(s) + CH_4(g) \rightarrow WC(s) + 2H_2(g)$$
⁽¹⁴⁾

Carburization depends on the atomic arrangement, the mass of the atom, and the temperature.⁴⁴ During the carburizing procedure, carbon may diffuse through and carburize the W lattices (Figure 2g). The exposed {110} facets are considered as ideal for carburization resistance as they possess high W surface densities and narrow empty channels for carbon diffusion. The resistance facilitates narrowing the WC layer, which would favor to reducing the oxygen adsorption free energy (Figure 1). The integrated mechanism for the formation of the W@WC with a dodecahedral microstructure proposed is shown schematically (Figure S6).

It is clear that H_2O plays a key role as a structure-directing agent by mediating the crystal growth of W along the {110} facets to form a stable dodecahedron shape. At the carburization stage, only a thin layer of WC was formed on the surface due to the aforementioned resistance of the {110} facets to carburization.

Transmission electron microscopy (TEM) of the product confirmed a core-shell structure of the W@WC (Figure 2e). The high-resolution TEM image (Figure 2f) taken on the edge of a particle (see the inset in Figure 2f) shows the exposed $\{001\}$, $\{100\}$, and $\{101\}$ facets of WC, thus confirming that the surface layer formed is the carbide. These results further confirm that the sample is composed of W and WC with a trace amount of W₂C as the intermediate layer (Figure 4a). The XRD data match the W@WC structural features observed in the TEM analysis. Scanning-TEM (STEM) and STEM-energy dispersive X-ray spectroscopy (STEM-EDS) (Figure S7) further confirm the formation of a uniform top layer of WC on the W core, with ca. 1:9 for the shell:core thickness ratio, in good agreement with the XRD and HRTEM results.

The physical-chemical stability of the W@WC determines the corrosion/oxidation resistance. As shown in the XRD pattern obtained following a second carburization process at 850 °C with dry CO/CO₂ (H₂O-free), the W diffractogram in the sample still remains (diffractogram 2 in Figure 4a), confirming good thermal stability of the W@WC. The resistance to carbon diffusion was clearly evidenced here from the presence of the dodecahedral W core which can only be formed in the presence of H₂O. A reference sample was synthesized by carburizing the same precursor with dry CO/ CO₂. The XRD, SEM, and pore size distribution data (Figure S8) indicate that the product consists of pure WC with a mesoporous structure. Significant thermal stability of the W@ WC in the air was evidenced by its high oxidation temperature. The weight gain associated with the oxidation of W@WC begins at ca. 602 °C, which is compared with ca. 475 °C found in the case of a pure WC sample (Figure S9a,b) and also 601 °C found in the case of a C protected WC sample.⁴⁵

Thermogravimetric analysis in the air was also used to determine the mass ratio of WC and W in the W@WC sample. Assuming all carbon being removed as CO_2 , the WC mass was calculated as follows

$$m_{\rm wc} + m_{\rm w} = m_{\rm i} \tag{15}$$

$$n_{\rm wc} \times \frac{M_{\rm WO_3}}{M_{\rm WC}} + m_{\rm w} \times \frac{M_{\rm WO_3}}{M_{\rm W}} = m_{\rm wo_3}$$
 (16)

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where m_i is the initial mass; m_{wc} is the mass of the WC shell; m_w is the mass of the tungsten core and m_{wo_3} is the mass of the oxidation product WO₃.

The TG data (Figure S9) showed a large mass gain of ca. 20.2 wt % $[(m_{wo_3} - m_i)/m_i]$ from which the WC content of the sample was estimated to be 20.5%.

As the aforementioned, if the trend of carbon atoms being transported outward was reduced by fabricating the W core with {110} facets, the carbon deficiency (W-terminated) is readily replaced by oxygen to keep the surface layer stable. After a period of time in the air, the surface compositional information on the prepared W@WC was analyzed by X-ray photoelectron spectroscopy (XPS). W, C, and O, due to the precursor and the carburization atmosphere, were all detected (Figure S10). The curve fitting of the W 4f spectral lines shows two principal peaks at 31.9 and 33.9 eV (Figure 4b) which are consistent with W $4f_{7/2}$ and $4f_{5/2}$ peaks, respectively, in WC.⁴⁶ Two other pairs of peaks at 35.9/32.5 eV and 38.0/34.5 eV were also observed which are in agreement with the $4f_{7/2}/4f_{5/2}$ binding energies of the +6 and +4 oxidation states of tungsten in WO₃ and WO₂, respectively, indicating the presence of WO_x sites on the surface of the WC shell. These results show evidence that, when an oxygen-containing species is present, the formation of tungsten oxycarbide species is possible.^{47,48} In this way, the surface vacancies can be maximally stabilized, where the O atoms diffuse into the second layer (becoming subsurface O) to replace the carbons that were bonded to the tungsten.

3.3. Catalytic Properties of W@WC Composite. The catalytic activity of the W@WC was tested for hydrogen evolution reaction (HER), which is a very important reaction in clean energy technologies and also an excellent probe reaction for studying multifunctional catalysts. The main results are shown in Figure 5 where the electrocatalytic performance toward HER can be assessed from the representative polarization curve obtained from the W@WC catalyst, in comparison with a commercial Pt/C catalyst (JM 20 wt % Pt on carbon) as well as nanosized and mesoporous WC samples, in 0.1 HClO₄ electrolyte solution; the typical cyclic voltammograms⁴⁹ of the W@WC catalyst and Pt/C are shown in Figure S11, confirming the clean surfaces were obtained before



Figure 5. Electrochemical polarization curves showing hydrogen evolution reaction over the W@WC, nanosized WC, mesoporous WC, Pt/C, and pristine CNT (carbon nanotube) in 0.1 $HClO_4$ solution (scan rate: 2 mV s⁻¹).

performing the corresponding polarization tests of HER as shown in Figure 5. As expected, the Pt/C catalyst exhibited a high catalytic performance for the HER with a reasonable low overpotential (η_i) of 245 mV $(\eta_i$ was defined as the potential applied at 50 mA cm⁻² of cathodic current density of HER), while the nanosized WC requires a much higher overpotential of 428 mV (green line; see Figure 5). Compared to nanosized WC, mesoporous WC exhibited a slightly lower η_i of 377 mV, which demonstrates that the presence of the mesoporous stucture favors proton reduction kinetics. Very interestingly, W@WC exhibited a much smaller η_i (283 mV; see red line, Figure 5) than both nanosized and mesorporous WC, indicating that the unique core-shell structure of W@WC reduces the extra (over)potential (and the corresponding energy) required for the HER. For driving a current density of 100 mA cm⁻², W@WC only required an overpotential of 337 mV, a performance which is comparable to Pt/C (with η_i value of 272 mV).

To get a fundamental understanding of the catalytic activity of W@WC toward HER, DFT atomistic modeling was performed. The free energy profiles in the hydrogen evolution reactions over WC, W@WC, and Pt surfaces were calculated and compared as shown in Figure 6. On the basis of these, the theoretical volcano curve between the hydrogen evolution reaction rate, $\ln(r_{\text{HER}})$, and atomic hydrogen adsorption free energy, $\Delta G(\text{H}^*)$, was plotted in Figure 7. It can be seen from Figure 7 that the position of the Pt(111) surface is near to the



Figure 6. Free energy (eV) profiles of the hydrogen evolution reactions on Pt(111), W(110)@WC_{1L}, W(110)@WC_{2L}, and WC(0001) surfaces.



Figure 7. Theoretical volcano curve between the hydrogen evolution reaction rate, $\ln(r_{\text{HER}})$, and atomic hydrogen adsorption energy, $\Delta G(\text{H}^*)$ (in eV).

top of the volcano curve with the hydrogen adsorption free energy of -0.21 eV (that is close to -0.06 eV of the top of the curve), indicating that Pt is very active for the hydrogen evolution reaction. However, on WC(0001), the hydrogen adsorption energy is -0.75 eV which being the highest of the four surfaces studied, resulting in the worst HER reaction rate. The hydrogen adsorption energies on $W(110)@WC_{1L}$ and W(110)@WC_{2L} surfaces are -0.39 and -0.46 eV, respectively, implying that they are significantly more active than WC(0001)with the two layers of the WC shell on the W core being slightly less active than the one layer of the WC shell on the W core; the latter is considerably close to Pt(111) (with a difference of only 0.18 eV). The optimized structures of hydrogen adsorption on WC(100)@WC_{1L}, WC(100)@WC_{2L}, and WC(0001) surfaces are shown in Figure S12, where H was adsorbed on the 3-fold hollow sites of W-terminated surfaces.

The W@WC composite has been further evaluated as a catalyst for another important reaction, the electroreduction of aromatic nitro-compounds under ambient conditions.^{50,51}

Herein, the as-prepared W@WC did exhibit a significant activity for nitrobenzene (NB) electrocatalytic reduction (Figure 8). As seen in Figure 8b, in which the main data obtained from W@WC, mesoporous WC, nanosized WC, W, and a commercial Pt/C catalyst are compared, while the corresponding cyclic voltammograms are shown in Figures 8a and S13, the W@WC displayed a comparable activity to that found for Pt/C for NB electroreduction, which is significantly higher than that observed from mesoporous WC, nanosized WC, and W.

The cathodic peak currents of NB reduction (on scanning the potential negatively) for the W@WC, meso-WC, nano-WC, W, and Pt/C electrodes are 21.11, 13.78, 6.09, 0, and 25.20 mA cm⁻², respectively (see also Table 1). Furthermore, for the W@ WC, the potential for the cathodic peak is shifted to a less negative voltage in comparison with the meso/nano-WC and Pt/C, i.e., -1.17 V for the W@WC compared with -1.29/-1.28 V for meso/nano-WC and -1.25 V for Pt/C. It is worth highlighting that the W@WC material demonstrates a higher activity for electrocatalytic reduction of NB than a mesoporous WC catalyst, even with only 1/12th the BET surface area of the meso-WC catalyst.

It is well-documented that the removal of O from the bulk or the nucleation of the metal phase becomes a rate-limiting factor only when enough $H_{(ads)}$ is available on the oxide surface.⁵² In this testing system, DMF and TBAP are attracted onto the WC



Figure 8. (a) Cyclic voltammograms (CVs) of the prepared W@WC sample in supporting electrolyte of 0.1 M TBAP in DMF solution without (curve: nitrobenzene-free) and with 0.03 M nitrobenzene, respectively; the scan rate is 50 mV s⁻¹. (b) Peak current and peak potential obtained from CV of the prepared W@WC in 0.1 M TBAP in DMF + 0.03 M nitrobenzene; also shown is the peak data obtained from CVs of a mesoporous WC, nanosized WC, W, and a Pt/C in 0.1 M TBAP in DMF + 0.03 M nitrobenzene, for comparison.

Table 1. Comparison of the BET Surface Area and Electrocatalytic Activity Data Obtained from the Cyclic Voltammetry of Nitrobenzene Electrochemical Reduction on the As-Prepared W@WC, Mesoporous WC, W, Nano-WC, and a Commercial Pt/C Catalyst

samples	$S_{\rm BET} \ ({\rm m}^2 \ {\rm g}^{-1})^a$	$i_p \text{ (mA cm}^{-2})$	E(V)
W@WC	0.51	21.11	-1.17
meso-WC	6.44	13.78	-1.29
Pt/C	commercial (234.10)	25.20	-1.25
W	1.46	0	
nano-WC	8.04	6.09	-1.28

^aBET surface area (S_{BET}) was calculated from the linear part of the BET plot.

surface, providing sufficient $H_{(ads)}$. During the cathodic potential scan, the O atoms on the surface were reduced at ca. -0.9 V (Figure S13c,d) and thus produced vacancies which could in turn coordinate the oxygen atom in the N=O group of NB.⁵³ The N=O bond was polarized and could be attacked and reduced easily by hydrogen atoms adsorbed on the WC at the negative potentials. During the potential cycling experiment, once a surface vacancy is created during the negative scan, the following positive sweep will facilitate the surface O recovering and diffusing to the surface vacancy, and filling it by cycle—forming the surface WC (Figure S13c).

4. CONCLUSION

In summary, a simple, yet efficient, one-pot synthesis method has been demonstrated to produce the novel W@WC coreshell architecture with a dodecahedral microstructure, by reducing and carburizing ammonium metatungstate under a CO/CO₂/H₂O atmosphere in one-pot reduction-carburization reactions. H₂O played a key role as a structure-directing agent by mediating the crystal growth of W along the $\{110\}$ facets to form a stable dodecahedron shape. At the carburization stage, only a thin layer of WC was formed on the surface due to the resistance of the {110} facets to carburization. The W@WC exhibited significant electrocatalytic activities toward both hydrogen evolution reaction (HER) and nitrobenzene electroreduction reaction, which being substantially higher than those found for meso- and nano-WC materials, and being comparable to those found for Pt/C. The experimental results on HER were explained by DFT calculations based on the energy profiles in the hydrogen evolution reactions over WC, W@WC, and Pt model surfaces. The W@WC also showed a high thermal stability and thus may serve as a promising more economical alternative to Pt catalysts in these important energy conversion and environmental protection applications. The current approach can be extended or adapted to various metals and carbides (see some examples in Figure S14), allowing for the design and fabrication of a wide range of catalytic and other multifunctional materials.

ASSOCIATED CONTENT

S Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acsami.7b04419.

Top and side views of W(100)@WC_{1L}, W(100)@WC_{2L}, and WC(0001) models used in DFT calculations, optimized structures of hydrogen adsorption on W(110)@WC_{1L},W(110)@WC_{2L}, and WC(0001) surfaces, schematic diagram of the experimental setup used, particle size distribution, SEM and STEM micrographs, simultaneous 2D STEM-EDS mapping, TG-DTA, XPS spectra of the W@WC and the contrast, CVs of W@WC, meso-WC, nano-WC, W, and Pt/C, and SEM images of MoC(Mo), W₂C, and Al samples (PDF)

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Notes

The authors declare no competing financial interest.

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