

Constitutive Relations for Reactive Transport Modeling: Effects of Chemical Reactions on Multi-Phase Flow Properties

Shuo Zhang^{a,*}, Hui-Hai Liu^a, Marinus I.J. van Dijke^b, Sebastian Geiger^b, Susan M. Agar^a

^a*Aramco Research Center-Houston, 16300 Park Row Dr. Houston, TX, 77084*

^b*Heriot-Watt University, Edinburgh, EH14 4AS, United Kingdom*

Abstract

The relationship between flow properties and chemical reactions is key to modeling subsurface reactive transport. This study develops closed-form equations to describe the effects of mineral precipitation and dissolution on multiphase flow properties (capillary pressure and relative permeabilities) of porous media. The model accounts for the fact that precipitation/dissolution only takes place in the water-filled part of pore space. The capillary tube concept was used to connect pore-scale changes to macroscopic hydraulic properties. Precipitation/dissolution induces changes in the pore radii of water-filled pores and consequently in the pore-size distribution. The updated pore-size distribution is converted back to a new capillary pressure-water saturation relation from which the new relative permeabilities are calculated. Pore network modeling is conducted on a Berea sandstone to validate the new continuum-scale relations. The pore network modeling results are satisfactorily predicted by the new closed-form equations.

Keywords: Mineral reactions, multiphase flow properties, reactive transport, constitutive relations

1. Introduction

In order to model geochemical reactions together with subsurface flow and solute transport, reactive transport modeling (RTM) is receiving increasing interest (Steefel et al., 2005). RTM refers to the creation of computer models that integrate chemical reactions with the transport of fluids through the Earth's crust. Such models predict the distribution in space and time of the chemical reactions that occur along a flow

*Corresponding author

Email address: shuo.zhang@aramcoservices.com (Shuo Zhang)

7 path. Today, RTM has become an essential tool for the analysis of coupled physical,
8 chemical, and biological processes in Earth systems. The advantage of this approach
9 is that it links individual time- and space-dependent processes in complex natural
10 systems.

11 In order to model hydro-geochemical problems on a large scale, RTM employs
12 continuum representations of the porous medium and assumes the existence of a rep-
13 resentative elementary volume where, for instance, flow can be described by Darcy's
14 law (Steefel et al., 2005). A porous medium is treated as continuous domains with
15 macroscopic flow and transport parameters such as hydraulic conductivity, porosity,
16 dispersivity, as well as geochemical parameters such as reactive surface area and reac-
17 tion rates. However, geochemical reactions such as mineral dissolution/precipitation
18 modify the porous medium's pore structure. An up-scaling procedure is needed to
19 predict changes in hydraulic properties such as permeability, capillary pressure, and
20 relative permeabilities within the framework of continuum-scale flow and transport
21 models.

22 Currently the effects of chemical reactions on flow properties are represented as a
23 relation between permeability and porosity in reactive transport modeling. Porosity is
24 updated after chemical calculations from the change of mineral volumes, then perme-
25 ability change is calculated from the porosity change using an empirical permeability-
26 porosity relation, most commonly the Carman-Kozeny relation (Kozeny, 1927; Car-
27 man, 1956), or the Verma and Pruess (1988) relation. To the best of our knowledge,
28 there are no closed-form relations available yet for the effects of chemical reactions
29 on multi-phase flow properties, and thus currently these effects cannot be accounted
30 for in reactive transport modeling.

31 This paper presents new constitutive relations to represent how chemical reac-
32 tions affect multi-phase flow properties on the continuum scale based on the con-
33 ceptual model of parallel capillary tubes. The parameters in our new relations are
34 either pre-existing input in a multi-phase flow simulation (initial capillary pressure
35 function), or intermediate modeling results (water saturation, changes in mineral vol-
36 ume). With those parameters the new relations can be implemented in an existing
37 reactive transport simulator directly, without introducing new variables.

38 The change of porosity, permeability, and multi-phase flow parameters due to
39 mineral reactions in a porous medium can be caused by different mechanisms in
40 different scenarios. For example, Pruess and Müller (2009) investigate permeability
41 change due to salt precipitation in the context of CO₂ injection. The rationale for
42 this process is that during CO₂ injection, water evaporates into the CO₂ stream.
43 Salinity starts to increase in the water and salt eventually precipitates out. Pruess
44 and Müller (2009) discuss how this 'dry out' will impact injectivity by modeling the
45 permeability change due to salt precipitation. Reduction of permeability can also be a
46 consequence of bacterial growth in a porous medium as a consequence of groundwater

47 recharge, water treatment or disposal processes, enhanced oil recovery schemes, or in-
48 situ bioremediation of organic contaminants in groundwater (Taylor and Jaffé, 1990;
49 Ginn et al., 2002; Schäfer et al., 1998). Plugging can be particularly severe for water
50 injection and bioremediation projects, since both processes inject water containing
51 relatively high levels of growth substrate and inorganic nutrients.

52 Mineral dissolution occurs where acid reacts with the surfaces of a porous medium.
53 A common method of stimulating oil wells to achieve greater production is to inject
54 acid into an oil bearing formation with the hope of significantly increasing the perme-
55 ability in some region around the wellbore. The reacting acid will dissolve a portion
56 of the porous solid thus changing the pore structure. The extent to which this disso-
57 lution of solid enhances permeability of the reservoir is essential to the design of an
58 effective acid treatment (Schechter and Gidley, 1969; Hiorth et al., 2010).

59 The relation between porosity change and permeability change is also relevant
60 to the effects of diagenesis such as cementation or dissolution on reservoir quality
61 prediction. Depending on the chemical and crystallographic properties, cements fill
62 the intergranular pores and increase the tortuosity of the permeable medium. The
63 result is a reduction in permeability compared to unaltered rock. The uncertainty of
64 the location and chemical composition of various cements makes it difficult to predict
65 their effects on permeability (Panda and Lake, 1995; Bjørkum and Nadeau, 1998).

66 This paper is intended to provide the fundamental basis for making reliable esti-
67 mates of the influence of pore structure on multi-phase flow properties. Our approach
68 should yield results pertinent to the problems cited above. Indeed, any problem con-
69 cerned with interaction of the porous solid-fluid system and its effects on multi-phase
70 flow properties should be susceptible to arguments similar to these presented here.

71 **2. Previous Relations**

72 Mineral dissolution and precipitation reactions in subsurface porous media alter
73 the structure of the pore network. The changes in pore structure manifest themselves
74 in the constitutive relations that characterize the continuum-scale properties of the
75 medium and are used in the governing equations of flow and transport. The question
76 is how these effects can be accurately captured in modeling reactive transport in
77 reservoirs.

78 The porosity changes caused by mineral reactions can be easily related to precipi-
79 tation or dissolution volume, but the permeability change associated with a change in
80 porosity is a more complex problem, as the porosity-permeability correlations depend
81 on many geometric factors such as pore-size distribution, pore shapes, and connec-
82 tivity. Since there is a wide variation in these geometric properties among natural
83 rock formations, the porosity-permeability correlations will generally depend on the
84 rock type and will be site specific. Attempts to obtain this relationship by many

85 investigators have produced results which differ considerably from each other. For
86 example, Mavis and Wilsey (1937) found the permeability of filter sands to be propor-
87 tional to ϕ^5 or ϕ^6 , while Brace (1977) found a 3rd power correlation with porosity for
88 crystalline rocks. It is therefore obvious that no simple general correlation between
89 porosity and permeability can be applied to all permeable materials. Xie et al. (2014)
90 discusses the implementation of permeability-porosity relationship in several reactive
91 transport codes and conducted benchmark problems, but only the Carman-Kozeny
92 relation is used in their models.

93 In fact we do not need an absolute permeability-porosity correlation but the re-
94 lationship between their relative changes. Many investigators have proposed such
95 relationships for different materials in which the porosity changes were brought about
96 by different physical mechanisms. The straight capillary models have been frequently
97 employed. Verma and Pruess (1988) assume that the medium has a set of non-
98 intersecting flow channels with either circular tubular or planar cross sections, and
99 construct series of models that are able to represent pore throat effects. Minor changes
100 in average porosity cause drastic permeability changes due to closure of the pore
101 throats in their model, and they find that there is a non-zero critical porosity ϕ_c at
102 which permeability reduces to zero.

103 The relations above assume that mineral dissolution and precipitation reactions
104 occur in all pores and ignore the important fact that for multiphase flow, these reac-
105 tions only occur in pores occupied by the water phase. For example, Ott et al. (2015)
106 observe in their CO₂ coring flooding experiment that precipitated salt occupies com-
107plementary space with initial CO₂ gas, and the overlap between salt precipitation and
108initial gas overlap less than 5%. As a result, these traditional approaches are appli-
109cable to the single-phase flow condition only, while multiphase flow is common in oil
110and gas reservoirs, geothermal reservoirs, geological carbon storage, and groundwa-
111ter remediation. Liu et al. (2013) use the concept of multi-phase flow in calculating
112the change of permeability due to a change in porosity. These authors argue that
113in multi-phase flow conditions, precipitation occurs only in the pore space occupied
114by brine, which corresponds to the small capillary tubes in the capillary tube model,
115since in most cases water is the wetting phase. They derive the relationship between
116permeability change and porosity change based on their conceptual model, and verify
117their predictions of new permeability with experimental results. However, although
118Liu et al. (2013) provide the relation of permeability change and chemical reactions,
119practical approaches to accurately estimate the effects of mineral dissolution and
120precipitation reactions on multiphase flow properties are not yet available.

121 This paper presents continuum-scale constitutive equations to calculate reaction-
122induced changes in capillary pressure and relative permeabilities. Section 3 presents
123the derivation of our new relationships. These new constitutive equations are fun-
124damentally based on the capillary tube concept. One assumption in this concept is

125 that the connectivity between pores in the rocks is represented by a group of capil-
126 lary tubes. To test whether this assumption will affect our predictions in changes of
127 capillary pressure and relative permeabilities, we present pore network modeling on a
128 Berea sandstone in Section 4 and compare the results with predictions from the new
129 continuum-scale equations.

130 The pore network models provide opportunities to study the change of hydraulic
131 properties due to reactions because detailed information is available at the pore scale
132 (Algive et al., 2012). Raouf et al. (2013) developed a pore-network modeling tool
133 capable of simulating fluid flow and multi-component reactive and adsorptive trans-
134 port under saturated and variably saturated conditions. Other researchers (Nogues
135 et al., 2013; Li et al., 2006; Varloteaux et al., 2013) have also developed similar reac-
136 tive transport models that are able to simulate the evolution of pore bodies within
137 a network. These models can be used to understand the evolution of porosity and
138 permeability in porous media at the pore scale, and aid in the representation of consti-
139 tutive relationships such as a porosity-permeability curve that can be used to model
140 larger scale processes in continuum scale models. However, to account for changes in
141 conductivity at the pore-to-pore level due to changes in the pore body volume due to
142 precipitation or dissolution of minerals, assumptions have to be made to correlate the
143 change in volume of the pores to a change in throat diameter. For example, in Nogues
144 et al. (2013), it is assumed that all pore throats are cylindrical in shape and have a
145 characteristic diameter, and mineral precipitation or dissolution simply reduces the
146 volume of the system and preferential precipitation/dissolution effects are not taken
147 into account. Thus the conclusions for the porosity-permeability relationship from
148 such models are mostly determined by how the pore-diameter change is related to
149 pore-volume change.

150 **3. Theory Development**

151 Our approach to derive the relation between chemical reactions and changes in
152 capillary pressure and relative permeabilities are shown in Fig.1 and described as
153 follows: starting with continuum-scale hydraulic properties, the pore size distribution
154 (PSD) function is calculated from the initial capillary pressure curve using the capil-
155 lary tube concept. Changes in mineral volume through equilibrium or kinetic mineral
156 reactions are then translated to changes in pore radii of the PSD by selectively chang-
157 ing the radii of water occupied pores. The resulting new PSD is converted back to an
158 updated capillary pressure curve, which is then used for computing total permeability
159 and relative permeabilities at the continuum scale. Note that our new development
160 is based on the Mualem (1976) or Van Genuchten (1980) model for capillary pressure
161 and relative permeability (before chemical reactions), but the procedure can be also
162 applied to other models.

163 *3.1. Change in Pore Size Distribution*

164 The pore space of a porous medium is conceptualized as cylindrical capillaries
 165 with a continuous distribution of radii r . A given capillary can be either water-filled
 166 or completely dry, depending on the saturation state of the medium. With this geo-
 167 metric idealization, the capillary pressure-water saturation curve can be interpreted
 168 to represent continuous cumulative pore-size distributions. In a given portion of the
 169 porous medium (in computational terms this would be a cell within the modeled do-
 170 main), at any time the water content is known. Due to precipitation/dissolution, the
 171 pore volumes and pore sizes will change and thus the capillary pressure curve changes
 172 also. The maximum radius up to which pores are water-filled and therefore affected
 173 by mineral reactions can be calculated from the capillary pressure head:

$$r = \frac{\zeta}{h} \quad (1)$$

174 where r is the radius of capillary tubes, h is the capillary pressure head corre-
 175 sponding to the current effective water saturation S , and ζ is the capillary factor
 176 $\zeta = \frac{2\sigma\cos\phi}{\rho g}$. Effective water saturation is defined as:

$$\bar{S} = \frac{S - S_r}{1 - S_r}, \quad (2)$$

178 where S is the wetting-phase saturation (the ratio of wetting-phase volume to the
 179 corresponding bulk volume of pore space), and subscript r refers to the residual water
 180 saturation.

182 The capillary pressure head h can be related to effective wetting-phase saturation
 183 by Van Genuchten (1980):

$$\bar{S} = [1 + (\alpha h)^n]^{-m}, \quad (3)$$

184 where α and $m=1-1/n$ are empirical parameters.

185 Before mineral reactions occur, the relative permeability of the wetting phase k_r
 186 can be expressed by Mualem (1976):

$$k_r = \bar{S}^{1/2} \left[\frac{\int_0^{\bar{S}} (1/h(x)) dx}{\int_0^1 (1/h(x)) dx} \right]^2. \quad (4)$$

187 Using the mathematical relation (Van Genuchten, 1980),

$$F(\bar{S}) = \frac{\int_0^{\bar{S}} (1/h(x)) dx}{\int_0^1 (1/h(x)) dx} = 1 - (1 - \bar{S}^{1/m})^m, \quad (5)$$

we have

$$k_r(\bar{S}) = \bar{S}^{1/2}[1 - (1 - \bar{S}^{1/m})^m]^2. \quad (6)$$

188 The changes in pore geometry during mineral precipitation or dissolution are
 189 complex. However, in order to obtain a closed-form result, we need to make some
 190 simplifications. Here we assume a strict dependency of mineral reactions on solution
 191 concentrations. In other words, the amount of dissolved or precipitated mineral in a
 192 given pore is linearly dependent on its pore volume. Also, we assume that the change
 193 in pore volume is uniform within a given pore.

194 If we denote the brine saturation at the time when mineral reaction starts as S_p ,
 195 then we can define the ratio of the pore volume after chemical reactions to that before
 196 reactions, β , as

$$\beta = \frac{S_p - S_{reaction}}{S_p}, \quad (7)$$

197 where $S_{reaction}$ is the content of precipitated or dissolved mineral, defined as the
 198 volume of mineral change divided by the bulk volume of pore space, and is positive
 199 for precipitation.
 200 for precipitation.

201 Given a porosity change from ϕ_0 to ϕ of a porous medium due to mineral disso-
 202 lution or precipitation, β can be calculated as

$$\beta = 1 - \frac{(\phi_0 - \phi)/\phi_0}{S_p}. \quad (8)$$

203 The ratio δ of the radius (for a pore after precipitation/dissolution) to its original
 204 radius can be approximated to be a power function of the corresponding volume ratio
 205 (Liu et al., 2013):

$$\delta = \frac{r^*}{r} = \beta^\chi, \quad (9)$$

206 where r^* is the radius after precipitation/dissolution, r is the original radius, and
 207 χ is an empirical parameter equal to 4.5. Liu et al. (2013) discussed this power law
 208 in detail. They selected the value of 4.5 to be consistent with patchy distribution
 209 of deposits, which was observed from scanning electron micrograph study where salt
 210 crystal did not distribute uniformly within a pore, but grew inwardly. Readers are
 211 referred to the Liu et al. (2013) paper and references therein.

212 In the previous study by Verma and Pruess (1988), changes in mineral volume
 213 were modeled as affecting the entire pore spectrum even though mineral reactions
 214 occur only in the water-filled part of the pore space. Here we only translate changes
 215 in mineral volumes to pore radii in the wet part of the porous medium.

In a given portion of the porous medium, at any time the water saturation is known. The maximum radius up to which pores are water-filled and therefore affected by mineral reactions is calculated by combining Eq.3 and Eq.1:

$$r_p = \alpha\zeta[\bar{S}_p^{-1/m} - 1]^{-1/n}. \quad (10)$$

216

217 The radius r_p divides the pore spectrum into a dry, inert part and a wet reac-
 218 tive part, which compensates for the change in mineral volume. For the calculation
 219 of the new PSD, only the pore radii of the wet pore space are multiplied by the
 220 proportionality factor δ .

221 3.2. Capillary Pressure

222 The calculation of change in capillary pressure after mineral reactions is straight-
 223 forward since capillary pressure is proportional to $1/r$.

Since the radius is changed from r to $r\delta$ for $S \leq S_p$ and remains unchanged for $S > S_p$, the new capillary pressure head is

$$h(S) = \begin{cases} \frac{h_0(S)}{\delta} & S \leq S_p, \\ h_0(S) & S > S_p \end{cases}, \quad (11)$$

224 where h_0 is the initial capillary pressure head at saturation S . This means that
 225 capillary pressure is increased by a factor of $1/\delta$ for $S \leq S_p$ in the case of precipitation
 226 ($\delta < 1$), and unchanged for $S > S_p$. Note that the new h - S curve is not continuous
 227 at $S = S_p$. This is because that mineral precipitation/dissolution only occurs in the
 228 water phase where $S \leq S_p$.

In the case of dissolution ($\delta > 1$), the sizes of the small pores initially occupied by water increase, and can potentially become larger than the previously large pores. Thus the pores need to be rearranged in terms of pore sizes to determine the new capillary pressure curve. If we follow the approach of the precipitation case, the new curve, which is a piecewise function, will have an offset at water saturation S_p using Eq.11, as indicated by the red dashed line in Fig.2. This means that some of the low saturations (S_1 to S_p) correspond to lower capillary pressures compared to some of the high saturations (S_p to S_2), which is physically not possible in the conceptual model of capillary tubes. In fact, some pores on the left side of S_p (S_1 to S_p) have larger pore sizes than some other pores on the right side (S_p to S_2), while water will always fill the small pores first. The pores whose sizes need to be rearranged in the new capillary curve lie between two threshold saturations, S_1 and S_2 , which correspond to capillary pressure heads δh_p and h_p/δ , where h_p is the capillary pressure head for

S_p in the initial capillary pressure curve. Thus, S_1 and S_2 can be calculated as

$$\begin{cases} S_1 = [1 + (\alpha h_p \delta)^n]^{-m} \\ S_2 = [1 + (\alpha h_p / \delta)^n]^{-m} \end{cases} \quad (12)$$

229 , where $h_p = h_0(S_p)$.

230 For $S < S_1$ and $S > S_2$, the new capillary pressure curve follows Eq.11. However,
 231 for $S_1 \leq S \leq S_2$, the capillary pressure curve needs to be adjusted. For a given
 232 capillary pressure head h ($h_p/\delta \leq h \leq h_p$), the water volume from h_p to h comes from
 233 two sources, the inert pores that have smaller pore radii than those corresponding
 234 to h (\hat{S}_2 to S_p), and the reactive pores whose sizes are enlarged but are still smaller
 235 compared to that corresponding to h (\hat{S}_1 to S_1). Thus,

$$S - S_1 = (\hat{S}_1 - S_1) + (\hat{S}_2 - S_p), \quad (13)$$

where $\hat{S}_1 = [1 + (\alpha h \delta)^n]^{-m}$ and $\hat{S}_2 = [1 + (\alpha h)^n]^{-m}$. Thus, the equation for the capillary pressure head after mineral dissolution is

$$S = \begin{cases} [1 + (\alpha h \delta)^n]^{-m} & h > h_p \\ [1 + (\alpha h \delta)^n]^{-m} + [1 + (\alpha h)^n]^{-m} - S_p & h_p/\delta < h \leq h_p \\ [1 + (\alpha h)^n]^{-m} & h \leq h_p/\delta \end{cases} \quad (14)$$

236 The values calculated from this final equation is plotted in Fig.2 as blue dashed
 237 line, where capillary pressure is a monotone function of water saturation. Note that
 238 here water saturation is written as a function of capillary pressure head, but capillary
 239 pressure head is not an explicit function of water saturation. This prevents us from
 240 obtaining closed-form equations for relative permeabilities for the dissolution case,
 241 which will be discuss later.

242 3.3. Permeability

243 The closed-form equation for permeability change due to mineral reactions is given
 244 in Liu et al. (2013) as follows:

$$\frac{K}{K_0} = \tau^{1/2} [(\delta - 1)(1 - (1 - \bar{S}_p^{1/m})^m) + 1]^2, \quad (15)$$

245

246 where τ is the tortuosity factor, and $\tau = 1 - \bar{S}_p + \delta^2 \bar{S}_p$. Liu et al. (2013) define this
 247 tortuosity factor to account for the fact that precipitated minerals impact tortuosity
 248 of porous media. This definition allows the tortuosity factor to have desirable values
 249 in two important cases: one for $\delta = 1$ (without precipitation) and $(1 - \bar{S}_p)^{1/2}$ for $\delta = 0$

250 Here we derive this relation using the pore size distribution (PSD) function $f(r)$,
 251 which will give us a slightly different result. The PSD function can be expressed by
 252 differentiation of the cumulative water content with respect to r (Ritter and Drake,
 253 1945). Before chemical reactions,

$$f(r) = \frac{d\theta(r)}{dr}. \quad (16)$$

254 We denote the new PSD function as $f^*(r^*)$, the new water content as θ^* , and the
 255 new radius as r^* . Recall that we defined the volume ratio before and after reactions
 256 as β , and the radius ratio as δ . Thus, we have $\theta^* = \theta\beta$, $r^* = r\delta$. For $r < r_p$, the new
 257 PSD function is

$$f^*(r^*) = \frac{d\theta^*(r^*)}{dr^*} = \frac{\beta}{\delta} f\left(\frac{r^*}{\delta}\right). \quad (17)$$

Following Liu et al. (2013), only the water occupied pores are modified,

$$\frac{K}{K_0} = \tau^{1/2} \left[\frac{\int_0^{r_p^*} r^* f^*(r^*) dr^* + \int_{r_p}^{\infty} r f(r) dr}{\int_0^{\infty} r f(r) dr} \right]^2, \quad (18)$$

258 where r_p is the threshold radius below which pores are occupied by water, and
 259 $r_p^* = r_p\delta$, which is the threshold radius post mineral reaction.

260 Substituting Eq.17 into Eq.18, we have

$$\frac{K}{K_0} = \tau^{1/2} \left[\frac{\int_0^{r_p} \delta\beta r f(r) dr + \int_{r_p}^{\infty} r f(r) dr}{\int_0^{\infty} r f(r) dr} \right]^2. \quad (19)$$

Using the mathematical relation (Van Genuchten, 1980),

$$F(\bar{S}) = \frac{\int_0^r r f(r) dr}{\int_0^{\infty} r f(r) dr} = 1 - (1 - \bar{S}^{1/m})^m, \quad (20)$$

we obtain

$$\frac{K}{K_0} = \tau^{1/2} [(\delta\beta - 1)(1 - (1 - \bar{S}_p^{1/m})^m) + 1]^2. \quad (21)$$

261 Comparing Eq.21 with Eq.15, the only difference is that Liu et al. (2013) misses
 262 a β term.

263 *3.4. Relative Permeability of Water*

264 Relative permeabilities are defined as the permeability of one phase divided by
 265 the saturated permeability, in our case, the saturated permeability of modified porous
 266 medium (K). However, for simplicity, we derive our new relative permeabilities as
 267 divided by the saturated permeability of the original porous medium (K_0). These
 268 relations can be corrected simply by using the factor K/K_0 as expressed in Eq.21.
 269 Let us denote the initial water permeability as K_{w0} , relative permeability as k_{w0} , and
 270 the new water permeability as K_w , relative permeability as k_w . Following Mualem
 271 (1976), we obtain

$$k_{w0} = \frac{K_{w0}}{K_0} = \tau^{1/2} \left[\frac{\int_0^r r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [F(\bar{S})]^2, \quad (22)$$

272 where $\tau = \bar{S}$.

273 When $S \leq S_p$, the new relative permeability of water is,

$$k_w = \frac{K_w}{K_0} = \tau^{1/2} \left[\frac{\int_0^r \delta\beta r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [\delta\beta F(\bar{S})]^2, \quad (23)$$

274 where $\tau = \delta^2 \bar{S}$.

Thus, the ratio of the new water relative permeability over the initial water relative permeability is,

$$\frac{k_w}{k_{w0}} = \delta^3 \beta^2. \quad (24)$$

When $S > S_p$,

$$k_w = \frac{K_w}{K_0} = \tau^{1/2} \left[\frac{\int_0^{r_p} \delta\beta r f(r) dr + \int_{r_p}^r r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)]^2, \quad (25)$$

275 where $\tau = \delta^2 \bar{S}_p + \bar{S} - \bar{S}_p$.

Thus,

$$\frac{k_w}{k_{w0}} = \left(\frac{\bar{S} - \bar{S}_p + \delta^2 \bar{S}_p}{\bar{S}} \right)^{1/2} \left[\frac{F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)}{F(\bar{S})} \right]^2. \quad (26)$$

To summarize, the new relation between relative permeability of the wetting phase and precipitation is:

$$\frac{k_w}{k_{w0}} = \begin{cases} \delta^3 \beta^2 & S \leq S_p \\ \left(\frac{\bar{S} - \bar{S}_p + \delta^2 \bar{S}_p}{\bar{S}} \right)^{1/2} \left[\frac{F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)}{F(\bar{S})} \right]^2 & S > S_p \end{cases}. \quad (27)$$

276 *3.5. Relative Permeability of Non-Wetting Phase*

277 Van Genuchten (1980) did not give the explicit formulation for the relative per-
 278 meability of non-wetting phase as a function of effective water saturation, but it is
 279 straightforward to derive this given the discussions above. Again, we denote the ini-
 280 tial permeability of the non-wetting phase as K_{g0} , relative permeability as k_{g0} , and
 281 the new permeability of the non-wetting phase as K_g , relative permeability as k_g .
 282 The integration for the relative permeability of non-wetting phase is from r to ∞ :

$$k_{g0} = \frac{K_{g0}}{K_0} = \tau^{1/2} \left[\frac{\int_r^\infty r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [1 - F(\bar{S})]^2, \quad (28)$$

283 where $\tau = 1 - \bar{S}$.

When $S \leq S_p$, the new relative permeability of non-wetting phase is,

$$k_g = \frac{K_g}{K_0} = \tau^{1/2} \left[\frac{\int_r^{r_p} \delta\beta r f(r) dr + \int_{r_p}^\infty r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [1 - \delta\beta F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)]^2, \quad (29)$$

284 where $\tau = (\bar{S}_p - \bar{S})\delta^2 + (1 - \bar{S}_p)$.

Thus,

$$\frac{k_g}{k_{g0}} = \left[\frac{(\bar{S}_p - \bar{S})\delta^2 + (1 - \bar{S}_p)}{1 - \bar{S}} \right]^{1/2} \left[\frac{1 - \delta\beta F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)}{1 - F(\bar{S})} \right]^2. \quad (30)$$

When $S > S_p$,

$$k_g = \frac{K_g}{K_0} = \tau^{1/2} \left[\frac{\int_r^\infty r f(r) dr}{\int_0^\infty r f(r) dr} \right]^2 = \tau^{1/2} [1 - F(\bar{S})]^2, \quad (31)$$

285 where $\tau = 1 - \bar{S}$.

Thus,

$$\frac{k_g}{k_{g0}} = 1. \quad (32)$$

To summarize, the new relation between relative permeability of the non-wetting phase and precipitation is:

$$\frac{k_g}{k_{g0}} = \begin{cases} \left[\frac{(\bar{S}_p - \bar{S})\delta^2 + (1 - \bar{S}_p)}{1 - \bar{S}} \right]^{1/2} \left[\frac{1 - \delta\beta F(\bar{S}) + (\delta\beta - 1)F(\bar{S}_p)}{1 - F(\bar{S})} \right]^2 & S \leq S_p \\ 1 & S > S_p \end{cases}. \quad (33)$$

286 4. Verification with Pore Network Modeling

287 In order to test the new equations for calculating changes of capillary pressure
288 and relative permeabilities due to mineral precipitation and dissolution, we use pore
289 network modeling (PNM) to compute these functions in a two-phase flow system.
290 The model comprises a constrained set of parameters that mimic the pore structure
291 of a porous medium.

292 PNM is commonly used to predict capillary pressure and relative permeability
293 functions for multi-phase flow simulations, and uses idealized geometric representa-
294 tions of complex pore structures and principles of percolation/invasion theory (Blunt,
295 2001; Blunt et al., 2013). It is a well-established approach for calculating the small-
296 scale petrophysical functions of two- and three-phase flow through porous media.
297 Here we use the pore-network model of Ryazanov et al. (2009). This model can be
298 applied to complex unstructured pore-networks, considers film and layer-flow using
299 thermodynamic criteria, uses a variety of shapes to represent the shapes of the pore
300 throats, and has been extensively validated using experimental data.

301 4.1. Initial Pore Network Model

302 We use a realistic 3D pore-network extracted from pore-space reconstruction meth-
303 ods and CT images that are geometrically and topologically equivalent to the pore
304 structures of a Berea sandstone sample (Fig.3). The network consists of 12349 pores
305 bodies (nodes) and 26146 pore throats (bonds). Each pore is assigned a regular shape
306 (triangle, star, or circle) based on the shape factor which best matches that of the
307 real pore shape. The average coordination number of this pore network is 4.19, initial
308 permeability is 1639.47 mD, and porosity is 0.24. In this numerical experiment, we
309 start with a fully water-saturated network ($S = 1.0$). Then, the non-wetting phase is
310 injected into the network for primary drainage. The pore network model calculates
311 the capillary pressure curve and relative permeability curves as a function of water
312 saturation through flooding. All floods are assumed to be capillary dominated and
313 are simulated according to invasion-percolation principles.

314 The initial capillary pressure curve and relative permeability curves are shown
315 in Fig.4 and Fig.5 for this pore network. They are calculated by running primary
316 drainage of non-wetting phase through an initially water-saturated sample. As can
317 be determined in Fig.4 and Fig.5, the residual saturation of water is 0.24.

318 In order to determine a reasonable value for the parameter m , we use Eq.3 to fit
319 the capillary pressure curve in Fig.4. Resulting parameters from fitting the capillary
320 pressure curve are $m = 0.748, \alpha = 0.0001994 Pa^{-1}$. To test this m value on the
321 relative permeability curves, we used Eq.6 and compared results with the relative
322 permeabilities calculated from pore network modeling. Results show that the van
323 Genuchten/Mualem model presents a satisfactory fit of initial capillary pressure and

324 relative permeability curves. We then use the value of m to predict how the capillary
 325 pressure curve and relative permeabilities change after chemical reactions, for a given
 326 amount of dissolved/precipitated minerals. The new capillary pressure and relative
 327 permeabilities are calculated from the initial values and the modification factors from
 328 our relations. The fitted initial van Genuchten/Mualem curves are not used in these
 329 calculation, thus do not affect the results. The main objective in the fitting process
 330 is to obtain the value of m which contains information on the shape of pore size
 331 distribution function, and is used in the relations.

332 4.2. Porosity-Permeability Relationship

333 For the purpose of comparing pore network modeling results with the new closed-
 334 form equations, we select two water saturations of 0.5 and 1.0 as the saturations
 335 at which mineral dissolution/precipitation occurs. Here we refer the two cases as
 336 the ‘new approach’ and the ‘traditional approach’ respectively since traditionally the
 337 relation between flow properties and chemical reactions are built on the assumption
 338 of full water saturation. In the new approach, we use the pore network model and
 339 run a primary drainage from the initial water-saturated condition to the target water
 340 saturation of 0.5. The bonds and nodes that are filled with water were identified
 341 in the pore network model when water saturation reaches $S_p = 0.5$. As shown in
 342 Fig.3, the red is the invaded non-wetting phase at $S_p = 0.5$, while the blue is water.
 343 Subsequently, the radii of the water-occupied bonds and nodes were modified by a
 344 factor of δ according to Eqs.7 and 9 for a given porosity change. In the traditional
 345 approach, the pore radii of all pores and throats are modified in the pore network
 346 model given the same amount of porosity change. This corresponds to the traditional
 347 assumption in which chemical reactions are considered to occur in all pores. The
 348 modified pore network models using both approaches were flooded again with non-
 349 wetting phase starting from a fully water saturated condition to calculate the new
 350 permeability, capillary pressure and relative permeability curves.

351 Fig.6 shows permeabilities of modified pore network models as a function of poros-
 352 ity change using the two approaches. The values of β are calculated from the poros-
 353 ity change using Eq.8 where $S_p = 0.5, \phi_0 = 0.24$. Given that $\beta \geq 0$, we have
 354 $\phi_{min}/\phi_0 = 1 - S_p = 0.5$, which means that porosity cannot drop below 50% of its
 355 original value given $S_p = 0.5$, because precipitation cannot be more than available
 356 pore volume. Ideally porosity does not have an upper limit due to dissolution. How-
 357 ever, since the current work only considers the change in pore size, it will not be
 358 valid when the porosity increase is large and pore structure is heavily modified. In
 359 fact, there will probably be wormholes forming when porosity increases substantially,
 360 which has not yet been well modeled. For the range of porosity depicted in Fig.6
 361 (0.19-0.27), the value of β ranges from 0.583 to 1.25, and the value of δ ranges from
 362 0.088 to 2.73.

363 In Fig.6 it can be observed that using the traditional approach in which precipi-
 364 tation is assumed to happen in all pores and throats, permeability decreases up to 3
 365 orders of magnitude when porosity decreases from 0.24 to 0.19. However, if precipi-
 366 tation is limited in the water occupied pores and throats, only the radii of the small
 367 pores and throats are decreased, while the other pores and throats remain unchanged.
 368 Thus permeability converges to a value which corresponds to all the unchanged pores
 369 and throats and does not decrease to zero. This is well captured by the present
 370 model, which we refer to as the modified Liu et al. (2013) model because the Liu
 371 et al. (2013) model only considered the change in radius but not in volume of the
 372 pores after mineral reactions as discussed in Section 3. The permeability change can
 373 be characterized into two regions, a transitional stage from porosity 0.24 to 0.22, and
 374 a plateau where permeability is relatively constant when porosity is smaller than 0.22.
 375 Most of the permeability is contributed from the unchanged pores and throats on this
 376 plateau. The traditional method which assumes that all pores and throats are filled
 377 by precipitations fails to capture this result.

378 4.3. Capillary Pressure and Relative Permeabilities

379 The predicted capillary pressure and relative permeabilities from pore network
 380 calculations are compared with our model in Figs.7-12. Two sets of calculations were
 381 conducted and compared. The first set of calculations assumes a decrease of porosity
 382 from 0.24 to 0.2015 ($\beta = 0.6795, \delta = 0.1757$), which represents precipitation, and
 383 the second set of calculations increases porosity from 0.24 to 0.2592 ($\beta = 1.160, \delta =$
 384 1.952), which represents dissolution. The dashed lines in all figures are the initial
 385 capillary pressure or relative permeabilities. The solid lines represent predictions
 386 from our current model and the dots are results from pore network modeling. The
 387 initial PNM data is used directly in our model and modifications of this data are
 388 applied after dissolution or precipitation based on our new relations.

389 In Fig.7, capillary pressure is increased by a factor of $1/\delta$ for water saturation
 390 smaller than 0.5, using the new approach, while remains unchanged for water satura-
 391 tion larger than 0.5, according to Eq.11. Thus, there is an offset at $S_w = 0.5$ that is
 392 well captured by our model and the pore network calculation. In Fig.8, the relative
 393 permeability of water is decreased by a factor of $\delta^3\beta^2$ for $S_w < 0.5$ according to Eq.27.
 394 Again, there is an offset at $S_w = 0.5$, and the change of relative permeability is less
 395 substantial for $S_w > 0.5$. The relative permeability of non-wetting phase in Fig.9 is
 396 unchanged for $S_w > 0.5$, but reduced for $S_w < 0.5$ according to Eq.33.

397 Fig.10-Fig.12 show the capillary pressure and relative permeability changes in the
 398 dissolution case, and the results from pore network models are well captured by our
 399 closed-form equations. Note that the relations of how relative permeabilities change
 400 after mineral dissolution is not given explicitly in this work, due to the fact that
 401 capillary pressure head cannot be written as an explicit function of water saturation

(Eq.14). In Fig.11 and 12 we adopted the relations for relative permeabilities in the precipitation case (Eq.27 and 33), and these relations fit the PNM data relatively well. In fact, Eq. 27 and 33 are valid in the dissolution case for $S < S_1$ and $S > S_2$ (Fig.2), since the $P_c - S$ relations are the same for dissolution and precipitation in these two regions. However, the interpolation between S_1 and S_2 will be slightly different. For permeability, the relation in the dissolution case is identical to the precipitation case. In the dissolution case, the pore sizes need to be rearranged to be consistent with the order of capillary tubes filled by water, from small to large. However, since permeability is calculated by integrating through all capillary tubes, the rearrangement does not affect the result. Thus the closed form relation for permeability change in the precipitation case can be directly used in the dissolution case.

In summary, the comparisons indicate that our proposed continuum-scale relations satisfactorily predict the pore-scale modeling results. The new method enables calculations of new permeability, capillary pressure and relative permeabilities in reservoir simulators after mineral reactions. It includes parameters that describe pore size distribution (m), the fraction of pore space that is water filled when precipitation happens (S_p), and the amount of precipitation/dissolution (δ, β). The related parameters are either model input (e.g., m), or intermediate modeling results (e.g., S_p), for calculating two-phase flow, so no new parameters need to be defined in reservoir simulators or reactive transport codes.

5. Discussions and Conclusions

The capillary tube model, which is the foundation of the presented model, has several underlying assumptions (Larson et al., 1981). One is that the connectivity of real porous media and the irregular geometry of real porous matrices and associated effects are ignored. Also this model neglects the water wetting films in pores filled by a non-wetting phase. Hence we cannot model how chemical components diffuse through these water films and eventually react with a (small) fraction of the pore space. Despite these shortcomings, the capillary tube model is widely applied as a simple link between continuum-scale hydraulic properties and PSD's (Taylor and Jaffé, 1990). In this paper we integrate the concept of modifying pore volumes through mineral reactions into more sophisticated pore network models to relate PSD's to capillary pressure curve and relative permeabilities. Comparisons between our capillary tube model and pore network model show that satisfactory predictions can be achieved using the capillary tube model for changes in capillary pressure, permeability and relative permeabilities.

The main contribution in this paper is the advancement of continuum-scale models for the effect of chemical reactions on multi-phase flow properties. One key step in reactive transport modeling is to capture these effects for feedbacks of chemical

440 reaction on fluid flow. Currently in most reactive transport simulators this is limited
441 to estimating permeability change from porosity change. However, due to the fact
442 that permeability is not a single function of porosity, but also a function of pore
443 geometry, the current approach has large uncertainties. In this paper, we adopt the
444 Liu et al. (2013) model for permeability change which not only considers porosity
445 change but also takes into account pore size distribution and water saturation. We
446 extend the Liu et al. (2013) model to multi-phase flow properties, and provide closed-
447 form equations on how capillary pressure and relative permeabilities should change
448 due to chemical reactions. These relations are continuum-scale equations, and can
449 be implemented in reactive transport models directly without introducing additional
450 parameters.

451 **References**

- 452 Algive, L., Békri, S., Nader, F. H., Lerat, O., Vizika, O., 2012. Impact of diage-
453 netic alterations on the petrophysical and multiphase flow properties of carbonate
454 rocks using a reactive pore network modeling approach. *Oil & Gas Science and*
455 *Technology—Revue d'IFP Energies nouvelles* 67 (1), 147–160.
- 456 Bjørkum, P. A., Nadeau, P. H., 1998. Temperature controlled porosity/permeability
457 reduction, fluid migration, and petroleum exploration in sedimentary basins. *AP-*
458 *PEA Journal* 38 (Part 1), 452–464.
- 459 Blunt, M. J., 2001. Flow in porous mediapore-network models and multiphase flow.
460 *Current opinion in colloid & interface science* 6 (3), 197–207.
- 461 Blunt, M. J., Bijeljic, B., Dong, H., Gharbi, O., Iglauer, S., Mostaghimi, P., Paluszny,
462 A., Pentland, C., 2013. Pore-scale imaging and modelling. *Advances in Water Re-*
463 *sources* 51, 197–216.
- 464 Brace, W., 1977. Permeability from resistivity and pore shape. *Journal of Geophysical*
465 *Research* 82 (23), 3343–3349.
- 466 Carman, P. C., 1956. *Flow of gases through porous media*. Academic press.
- 467 Ginn, T. R., Wood, B. D., Nelson, K. E., Scheibe, T. D., Murphy, E. M., Clement,
468 T. P., 2002. Processes in microbial transport in the natural subsurface. *Advances*
469 *in Water Resources* 25 (8), 1017–1042.
- 470 Hiorth, A., Cathles, L., Madland, M., 2010. The impact of pore water chemistry on
471 carbonate surface charge and oil wettability. *Transport in porous media* 85 (1),
472 1–21.

- 473 Kozeny, J., 1927. Über kapillare Leitung des Wassers im Boden:(Aufstieg, Ver-
474 sickerung und Anwendung auf die Bewässerung). Hölder-Pichler-Tempsky.
- 475 Larson, R., Scriven, L., Davis, H., 1981. Percolation theory of two phase flow in
476 porous media. *Chemical Engineering Science* 36 (1), 57–73.
- 477 Li, L., Peters, C. A., Celia, M. A., 2006. Upscaling geochemical reaction rates using
478 pore-scale network modeling. *Advances in water resources* 29 (9), 1351–1370.
- 479 Liu, H.-H., Zhang, G., Yi, Z., Wang, Y., 2013. A permeability-change relationship
480 in the dryout zone for CO_2 injection into saline aquifers. *International Journal of*
481 *Greenhouse Gas Control* 15, 42–47.
- 482 Mavis, F., Wilsey, E., 1937. Filter sand permeability studies. *Eng. News Rec* 118,
483 299–300.
- 484 Mualem, Y., 1976. A new model for predicting the hydraulic conductivity of unsatu-
485 rated porous media. *Water Resour. Res* 12 (3), 513–522.
- 486 Nogues, J. P., Fitts, J. P., Celia, M. A., Peters, C. A., 2013. Permeability evolution
487 due to dissolution and precipitation of carbonates using reactive transport modeling
488 in pore networks. *Water Resources Research* 49 (9), 6006–6021.
- 489 Ott, H., Roels, S., De Kloe, K., 2015. Salt precipitation due to supercritical gas
490 injection: I. capillary-driven flow in unimodal sandstone. *International Journal of*
491 *Greenhouse Gas Control* 43, 247–255.
- 492 Panda, M. N., Lake, L. W., 1995. A physical model of cementation and its effects on
493 single-phase permeability. *AAPG bulletin* 79 (3), 431–443.
- 494 Pruess, K., Müller, N., 2009. Formation dry-out from CO_2 injection into saline aquifers:
495 1. effects of solids precipitation and their mitigation. *Water Resources Research*
496 45 (3).
- 497 Raouf, A., Nick, H., Hassanizadeh, S., Spiers, C., 2013. Poreflow: A complex pore-
498 network model for simulation of reactive transport in variably saturated porous
499 media. *Computers & Geosciences* 61, 160–174.
- 500 Ritter, H., Drake, L., 1945. Pressure porosimeter and determination of complete
501 macropore-size distributions. pressure porosimeter and determination of complete
502 macropore-size distributions. *Industrial & Engineering Chemistry Analytical Edi-*
503 *tion* 17 (12), 782–786.

- 504 Ryazanov, A., Van Dijke, M., Sorbie, K., 2009. Two-phase pore-network modelling:
 505 existence of oil layers during water invasion. *Transport in Porous Media* 80 (1),
 506 79–99.
- 507 Schäfer, D., Schäfer, W., Kinzelbach, W., 1998. Simulation of reactive processes re-
 508 lated to biodegradation in aquifers: 1. structure of the three-dimensional reactive
 509 transport model. *Journal of contaminant Hydrology* 31 (1), 167–186.
- 510 Schechter, R., Gidley, J., 1969. The change in pore size distribution from surface
 511 reactions in porous media. *AIChE Journal* 15 (3), 339–350.
- 512 Steefel, C. I., DePaolo, D. J., Lichtner, P. C., 2005. Reactive transport modeling:
 513 An essential tool and a new research approach for the earth sciences. *Earth and
 514 Planetary Science Letters* 240 (3), 539–558.
- 515 Taylor, S. W., Jaffé, P. R., 1990. Biofilm growth and the related changes in the physi-
 516 cal properties of a porous medium: 1. experimental investigation. *Water Resources
 517 Research* 26 (9), 2153–2159.
- 518 Van Genuchten, M. T., 1980. A closed-form equation for predicting the hydraulic
 519 conductivity of unsaturated soils. *Soil science society of America journal* 44 (5),
 520 892–898.
- 521 Varloteaux, C., Békri, S., Adler, P. M., 2013. Pore network modelling to determine
 522 the transport properties in presence of a reactive fluid: From pore to reservoir scale.
 523 *Advances in Water Resources* 53, 87–100.
- 524 Verma, A., Pruess, K., 1988. Thermohydrological conditions and silica redistribution
 525 near high-level nuclear wastes emplaced in saturated geological formations. *Journal
 526 of Geophysical Research: Solid Earth (1978–2012)* 93 (B2), 1159–1173.
- 527 Xie, M., Mayer, K. U., Claret, F., Alt-Epping, P., Jacques, D., Steefel, C., Chiaberge,
 528 C., Simunek, J., 2014. Implementation and evaluation of permeability-porosity and
 529 tortuosity-porosity relationships linked to mineral dissolution-precipitation. *Com-
 530 putational Geosciences*, 1–17.

531 **Nomenclature**

- 532 \bar{S} Effective water saturation
- 533 β Ratio of pore volume after reactions to before reactions

534	ϕ	Porosity after reactions
535	ϕ_0	Initial porosity
536	τ	Tortuosity
537	h	Capillary pressure head
538	K	Permeability after reactions
539	K_0	Initial permeability
540	K_{g0}	Initial gas permeability
541	k_{g0}	Initial gas relative permeability
542	K_g	Gas permeability after reactions
543	k_g	Gas relative permeability after reactions
544	K_{w0}	Initial water permeability
545	k_{w0}	Initial water relative permeability
546	K_w	Water permeability after reactions
547	k_w	Water relative permeability after reactions
548	m	Empirical parameter in the van Genuchten $h - S$ relation
549	r	Radius of capillary tube
550	r^*	Radius after reactions
551	r_p	Maximum radius up to which pores are water-filled
552	S	Water saturation
553	S_p	Water saturation when mineral reaction occurs
554	S_r	Residual water saturation

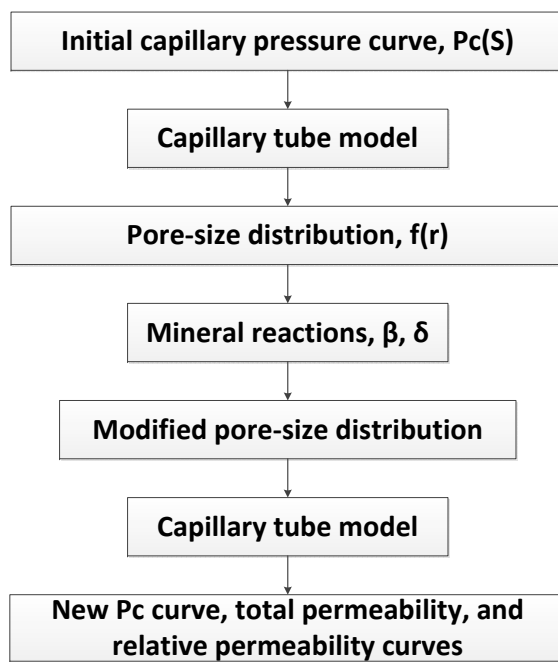


Figure 1: Work flow to develop new constitute relations for multi-phase flow properties and chemical reactions.

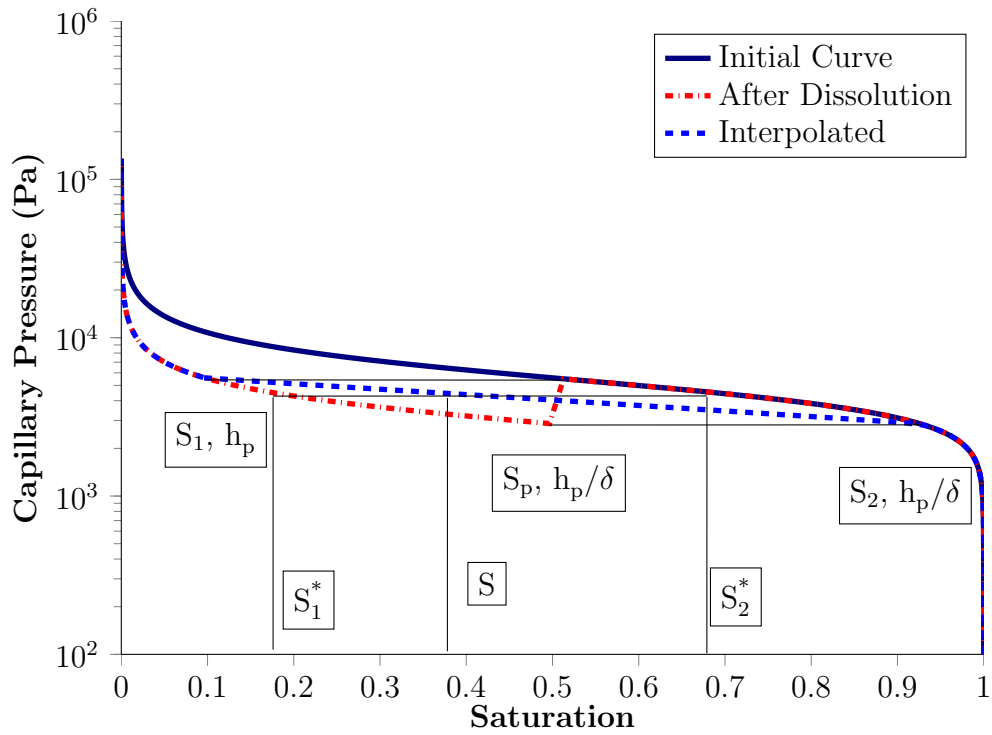


Figure 2: Change of capillary pressure curve after mineral dissolution. Red dash-dot line illustrates the approach used in the precipitation case, which gives un-physical results in the dissolution case. Blue dashed line represents the correct new capillary pressure curve as described by Eq.14. For any capillary pressure head h on the new curve, its saturation S can be determined from volume balance (Eq.13).

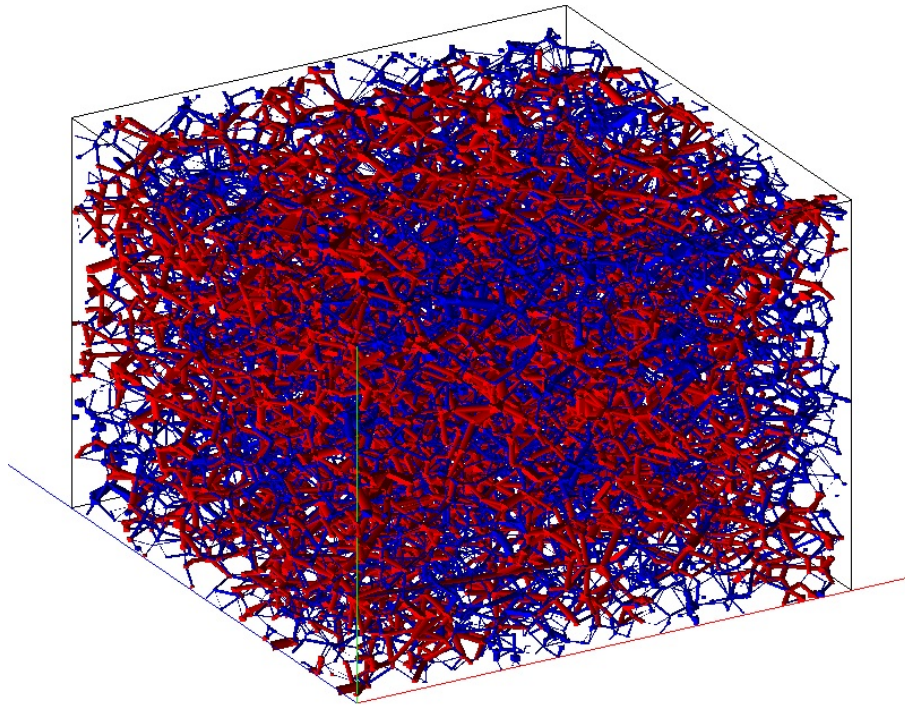


Figure 3: Snap shot of the Berea pore network model at water saturation of 0.5. Blue color represents water, red color represents the non-wetting phase. Size of the model is 2.14 mm x 2.14 mm x 2.14 mm.

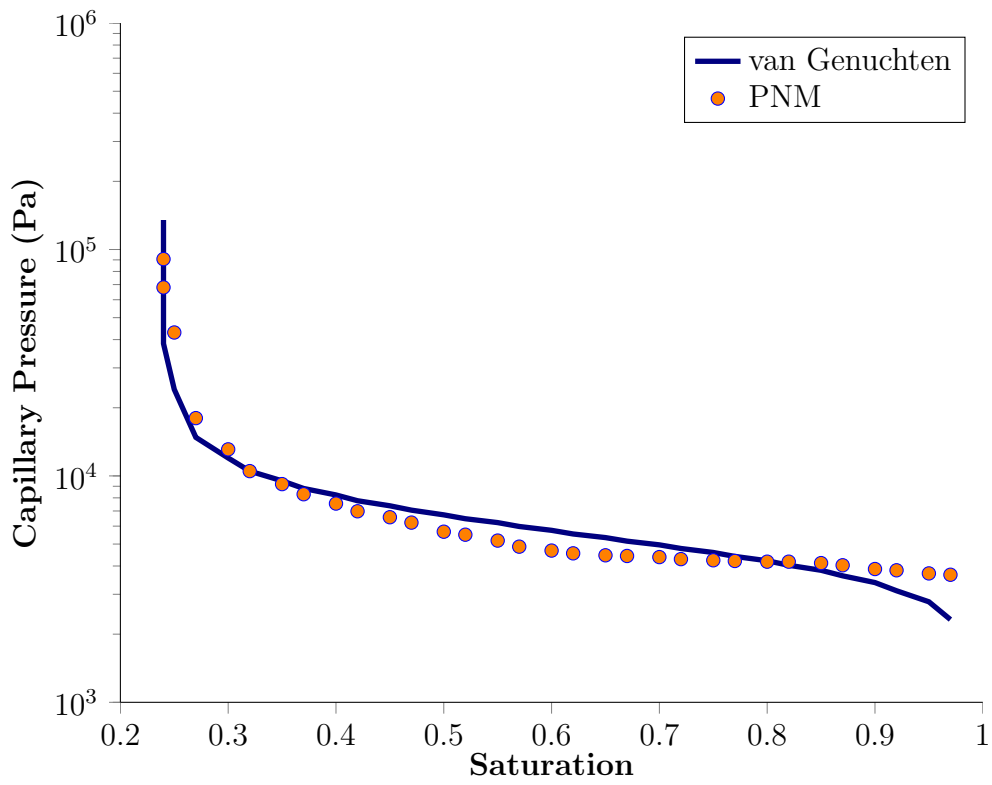


Figure 4: Initial capillary pressure data from pore network modeling and fitting with van Genuchten relation.

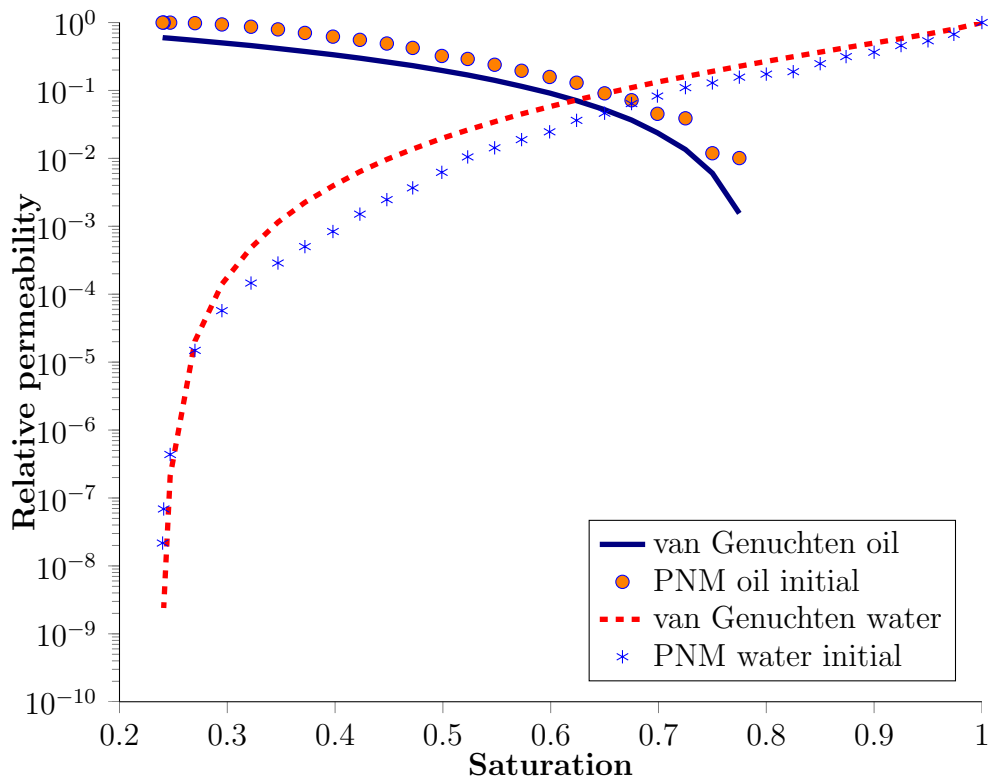


Figure 5: Initial relative permeabilities of water and non-wetting phase from pore network modeling and comparison with van Genuchten relations using parameters from 4.

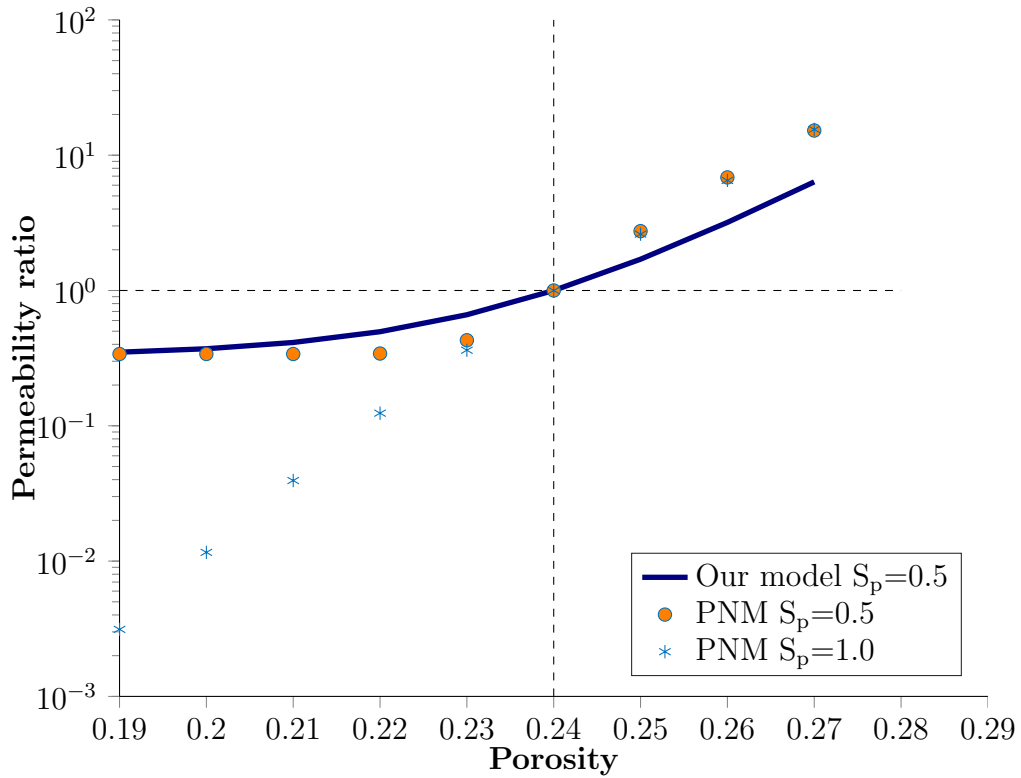


Figure 6: Permeability change as a function of porosity change predicted from current model and pore network modeling ($S_p = 0.5$), compared with traditional approach where all pores and throats are assumed to have chemical reactions ($S_p = 1.0$). In our model, $S_p = 0.5$, $\phi_0 = 0.24$, the value of β ranges from 0.583 to 1.25, and the value of δ ranges from 0.088 to 2.73.

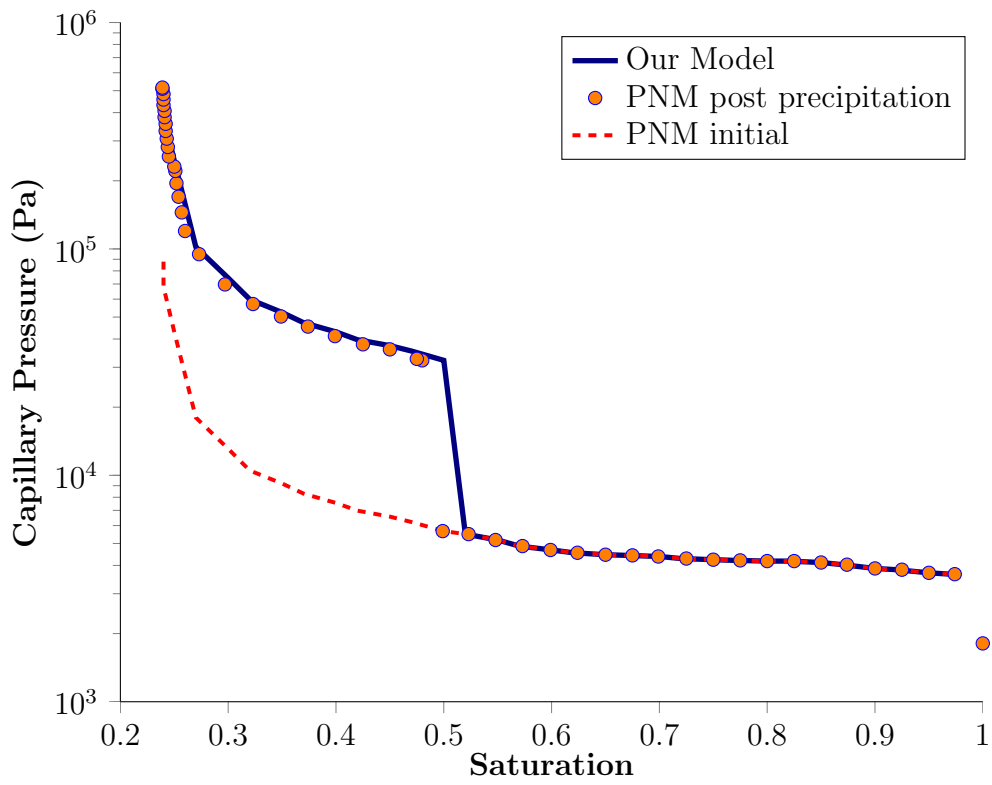


Figure 7: New capillary pressure curve after mineral precipitation predicted from our model and comparison with pore network modeling, using the new approach.

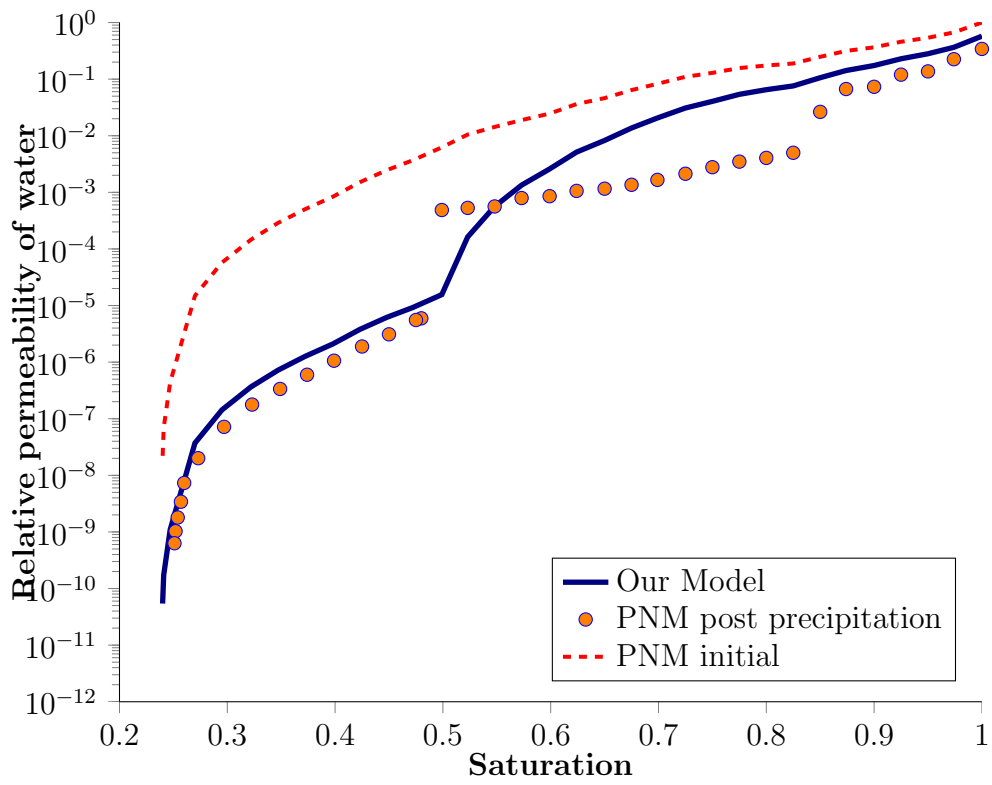


Figure 8: New water relative permeability curve after mineral precipitation predicted from our model and comparison with pore network modeling, using the new approach.

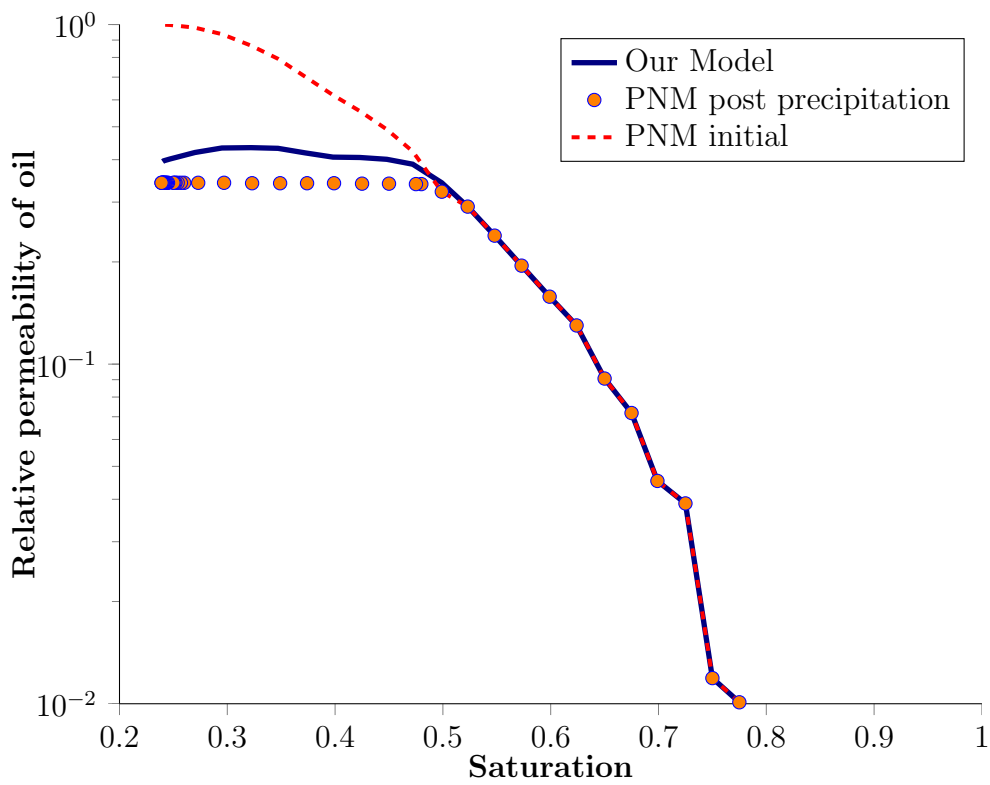


Figure 9: New relative permeability of the non-wetting phase after mineral precipitation predicted from our model and comparison with pore network modeling, using the new approach.

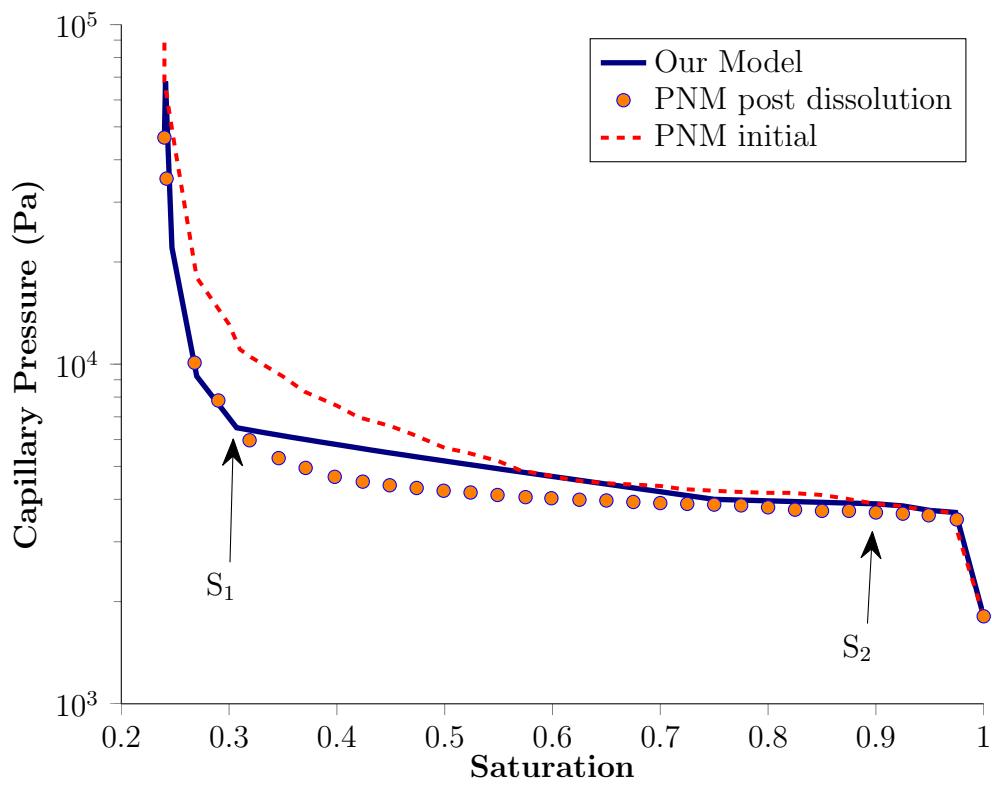


Figure 10: New capillary pressure curve after mineral dissolution predicted from our model and comparison with pore network modeling, using the new approach.

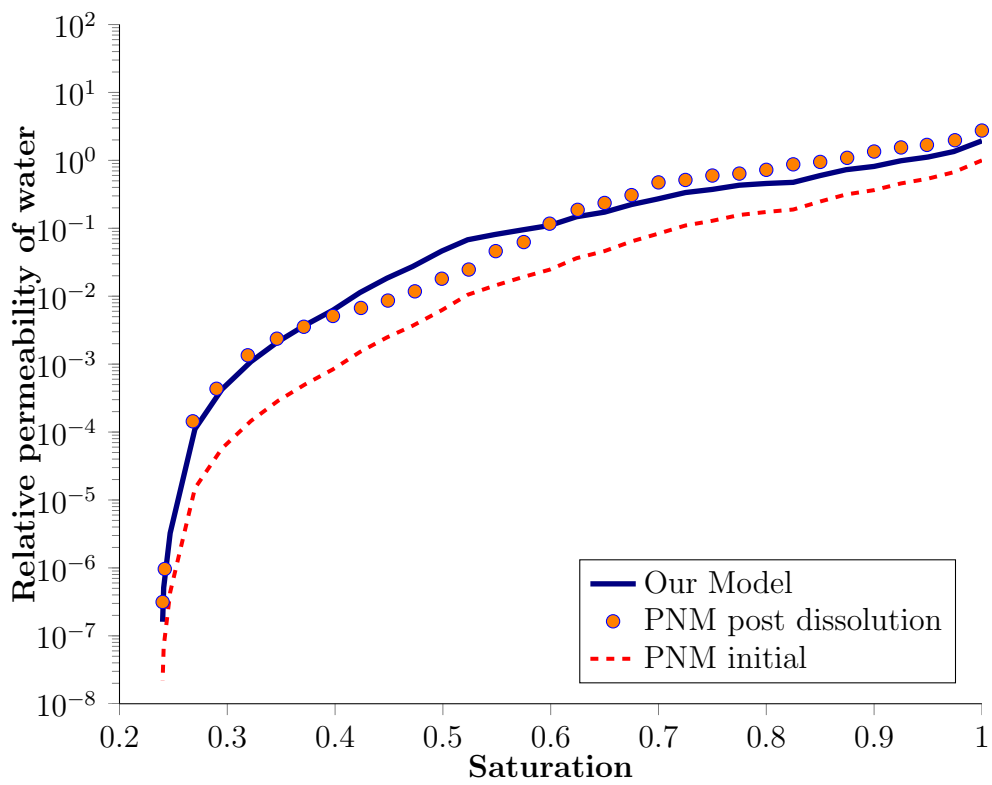


Figure 11: New water relative permeability curve after mineral dissolution predicted from our model and comparison with pore network modeling, using the new approach.

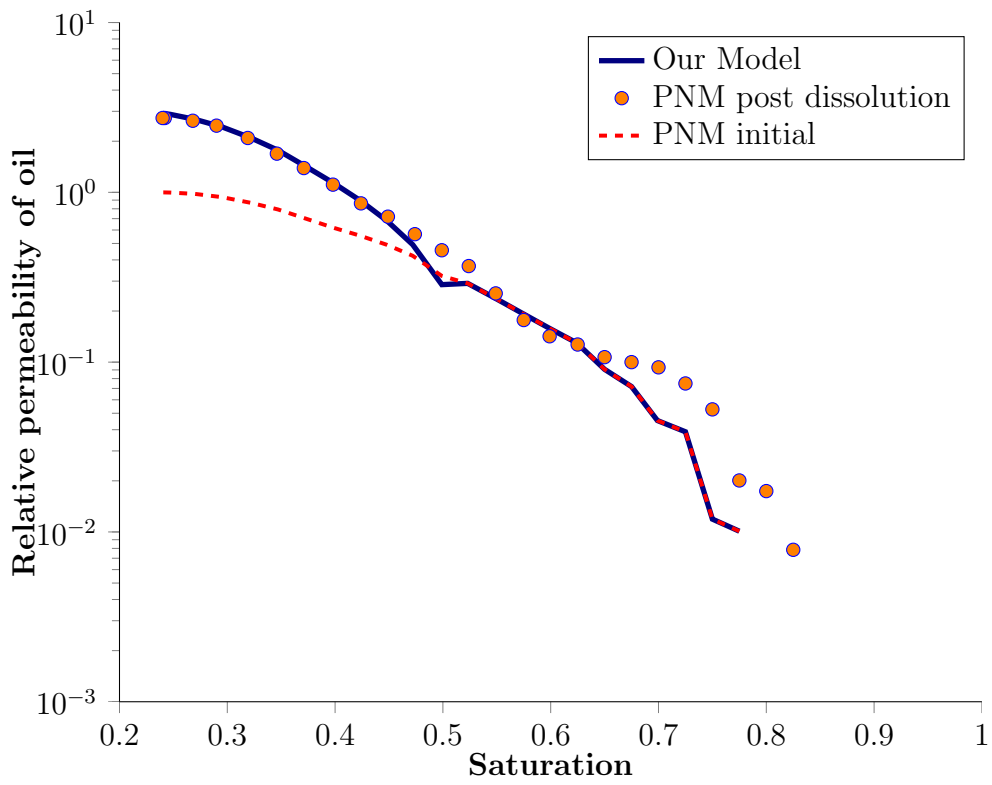


Figure 12: New relative permeability curve of the non-wetting phase after mineral dissolution predicted from our model and comparison with pore network modeling, using the new approach.