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Inactivation of bacteria in seafood processing water by means of UV treatment

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7

8 ABSTRACT

Seafood processing is a large-scale food industrial activity, in the UK and worldwide, which 9 requires substantial quantities of clean water for washing purposes. Therefore, the aim of this 10 study is to assess the feasibility of ultraviolet (UV) treatment to disinfect water coming from 11 shellfish washing process, as to safely recycle it in the process. For this reason, different 12 operating parameters that typically affect UV treatment efficiency, namely the power output 13 of the UV lamp (5W, 9W, and 11W), the turbidity of the washing water (0 - 52 NTU), and 14 the initial bacterial concentration $(10^4, 10^5, 10^6 \text{ CFU mL}^{-1})$ were studied. Water disinfection 15 was monitored by following changes in the concentration of the Escherichia coli (E. coli) 16 17 bacteria. Photoreactivation of bacteria after UV disinfection was also investigated. Results showed that the UV treatment can efficiently inactivate bacteria in shellfish processing water, 18 since E. coli (10^6 CFU mL⁻¹) in turbid (i.e. 0.074 - 35 NTU) seafood processing water were 19 inactivated within the first 15 sec of treatment, by means of an 11 W germicidal lamp. Under 20 21 these conditions, no bacteria photoreactivation was observed after 2 h of exposure to natural 22 light. The disinfection efficiency was decreased when the initial bacterial concentration and water turbidity were increased. In addition, the increase of UV power output resulted in a 23 substantial increase of bacterial inactivation. Furthermore, E. coli were reactivated after 2 h 24 of exposure to natural light when the turbidity of the washing water was ≥ 42 NTU or when 25 the initial bacterial concentration was high (i.e. 10^5 and 10^6 CFU mL⁻¹). 26

27

28 **KEYWORDS:** shellfish; seafood processing industry; water disinfection; aquaculture; water

29 recycling

30 **1. Introduction**

Shellfish farming and packaging is a large-scale food industrial activity in the UK and 31 worldwide. The UK exports most of the seafood it harvests, thus resulting to high economic 32 gains (e.g. in 2011 just over 435,000 tonnes of seafood, worth £1.46 billion, were exported 33 from the UK (Seafish, 2012a)). High value shellfish, such as langoustine, crab and scallops, 34 are exported to the French, Spanish and Italian markets (Seafish, 2012a). Moreover, Scotland 35 dominates the UK seafood processing industry, while secondary processing units are found in 36 the North England and Wales, thus providing 11,864 full-time jobs in 325 units throughout 37 38 the UK (data for 2011) (Seafish, 2012a, b). To maintain the high quality and profitability of the UK shellfish species, domestic suppliers have focused on improving the sustainability of 39 40 their farming, as well as their packaging process.

41 Shellfish packaging requires vigorous washing and scrubbing with clean water, as to ensure 42 maximum removal of sediments and other debris. Water should be taken from an appropriate source, which is usually sea or tap water (MassachusettsGeneralLaws, 2015). Nonetheless, 43 44 seawater pumping is an energy intensive process, while also it may be inappropriate due to high pollution levels. It has been extensively reported that seawater in the European continent 45 46 and worldwide face great challenges due to heavy metal (Besada et al., 2011; Kallithrakas-Kontos and Foteinis, 2015; Wang et al., 2013) and oil pollution (Cohen, 2013). Moreover, 47 many seafood processing industries are sited inland, therefore seawater utilization is 48 unpractical. In these cases, tap water is the only solution, but its use can significantly increase 49 50 operational costs and negatively affect the sustainability of the process. Furthermore, shellfish processing machinery consumes large amounts of water (e.g. for shellfish washing, 51 equipment and floor cleaning), while water reclamation and recycling is not applied. 52 Therefore, water minimization and reuse strategies should be introduced in such industries, as 53 to make seafood washing more efficient and sustainable; thus improving their overall 54 55 environmental footprint, competitiveness and profitability.

Ultraviolet (UV) irradiation is a well-established treatment technology for bacterial inactivation in water, air and solid surfaces and is one of the approved technologies used for food processing and preservation (EPA, 2006; Gardner and Shama, 1999; Quek and Hu, 2013; Venieri et al., 2013). The efficiency of UV treatment is attributed to the hazardous effects of UV-C radiation, which can destroy directly the DNA and the outer cell membrane of pathogenic microorganisms (Chatzisymeon et al., 2011; Venieri et al., 2013). UV-C irradiation between 250 nm and 270 nm, where the maximum absorbance of nucleotide bases 63 of the genome occurs, including thymine, cytosine and uracil, can induce damages in DNA and RNA, thus inhibiting cell transcription and replication (Vélez-Colmenares et al., 2012). 64 Specifically, the major DNA lesion, induced by germicidal UV-C irradiation at 254 nm, is the 65 formation of pyrimidine dimers. The presence of these lesions inhibits the normal replication 66 of DNA, and therefore results in inactivation of the microorganisms in short time periods 67 (Nebot Sanz et al., 2007). In addition, UV disinfection does not require chemical reagents, 68 69 thus another advantage is that there is no formation of hazardous disinfection by-products after treatment (Summerfelt, 2003). However, its main drawback is that many 70 microorganisms, including bacteria, are known to possess the ability to repair their DNA 71 damage in the presence (photoreactivation) or absence (dark repair) of light (EPA, 2006; 72 Nebot Sanz et al., 2007; Quek and Hu, 2013; Sinha and Hader, 2002). This can lead to the 73 reactivation of bacteria, after UV treatment, hence affecting disinfection efficiency and 74 rendering UV treatment unsafe. Till now, few studies have dealt with the use of UV 75 irradiation for food processing, including the inactivation of bacteria on raspberries and 76 strawberries (Bialka et al., 2008), in fruit juices (Gayán et al., 2012; Müller et al., 2011; 77 Santhirasegaram et al., 2015), apple cider (Unluturk et al., 2004), goat milk (Kasahara et al., 78 2015), and in liquid egg products (Unluturk et al., 2008). However, to the best of the author's 79 80 knowledge, there is no study dealing with the application of UV for the treatment of seafood processing waters. 81

Therefore, the aim of this study is to investigate the feasibility of the UV method to disinfect shellfish washing water, thus being able to safely recycle treated water in the process. For this purpose, washing water from a shellfish processing industry was used and various operating parameters that typically affect UV efficiency were studied. These were the lamp power output, the initial bacterial concentration, water turbidity and treatment time. The effect of bacterial photoreactivation on treatment durability was also examined, as to ensure the feasibility of the process.

89

90 2. Materials and Methods

91 **2.1. Shellfish processing water**

92 Shellfish processing water was collected from an industry that uses tap water for shellfish93 washing, located in the UK. The processing water originates from the industry's shellfish

94 washing line, where tap water is initially used and then it is collected in tanks (about 250 L) and reused, if appropriate, in the washing process. However, shellfish-associated bacteria, 95 including potential pathogens and spoilage organisms, build up in the tanks, thus rendering 96 the used water inadequate for recycling purposes after a short period of time. Therefore, this 97 water has to be disposed of, about every 10 min, when the bacterial concentration becomes 98 too high. thus preventing the efficient water recycling in the washing stage, and fresh tap 99 100 water needs to be introduced in the system. Shellfish-associated bacteria can include Vibrio and Shigella species, Salmonella, or other toxin-forming bacteria (Iwamoto et al., 2010). In 101 102 this work, water disinfection was monitored by following changes in the E. coli bacteria, which is a common and very popular indicator pathogenic microorganism for potable water 103 (Chatzisymeon et al., 2011), since according to current legislation the quality of seafood 104 washing water should follow the standards of drinking water (MassachusettsGeneralLaws, 105 2015). 106

In order to measure bacterial contamination in the used washing water and assess the feasibility of the UV treatment, tap water was continuously (i.e. every 10 min) recycled in the shellfish washing line for up to 40 min. Washing water samples were withdrawn after 10, 20, 30, and 40 min of washing, as to measure their physicochemical and microbiological characteristics. The water samples were collected in sterilized sampling bottles of 1 L, kept at 4 °C and immediately dispatched for further analyses. After measuring their characteristics, samples were sterilized at 121 °C for 15 min and kept in the fridge (4 – 8 °C).

114

115 **2.2. Bacterial strain**

The bacterial strain of *Escherichia coli*, which was used in this work as a water quality 116 117 indicator, was isolated from the shellfish washing waters by membrane filtration. From the collected samples 200 µL were passed through a 0.45 µm pore-sized filter (cellulose 118 acetate/nitrate membranes by Sigma-Aldrich), using a vacuum pump VP series (KNF Lab). 119 These membranes were aseptically placed up on plates with Brilliance E. coli/Coliform Agar 120 (Oxoid) selective media, thus ensuring that no air bubbles were trapped. The plates were 121 incubated at 37 °C for 20 – 24 hours and E. coli colonies with purple-blue colour were picked 122 for further use. Specifically, the isolated *E. coli* were spiked into the sterile industrial washing 123 water to achieve the desired initial bacterial loading for each experimental run. The standard 124 E. coli ATCC 23716 (American Type Culture Collection, Rockville, MD, USA) strain was 125

also used. The freeze-dried cultures were rehydrated and reactivated according to the manufacturer's instructions. The concentration of bacterial cells in the shellfish processing water ranged from 10^4-10^6 CFU mL⁻¹, as estimated by measuring its optical density at 600 nm on a Cary100 UV-Vis double-beam (Varian, Inc.) spectrophotometer.

130

131 2.3. UV experiments

Experiments were conducted in an immersion well, batch type, laboratory scale photoreactor 132 shown in Schematic 1. This is a two compartment apparatus and consists of an inner quartz 133 glass housing the lamp and an exterior cylindrical reaction vessel made of borosilicate glass. 134 The reaction mixture was placed in the exterior cylindrical reaction vessel (compartment 1) 135 and the inner quartz glass was immersed inside the reaction mixture. The UV lamp was 136 placed inside the inner glass tube (compartment 2). It should be noted that this apparatus was 137 constructed and assembled in the workshop of the University of Edinburgh, UK. In a typical 138 experimental run, 300 mL of the shellfish processing water were introduced in the reaction 139 vessel. The bacterial suspension was magnetically stirred, to ensure complete mixing of E. 140 141 *coli* with the processing water, and then the UV lamp was turned on. UV-C irradiation, with emission wavelength at 254 nm, was provided by an 11 W (11TUV, PL-S, Philips) or a 9 W 142 (PL, 2 PIN, Philips) or a 5 W (5TUV, PL-S, 2G7 base, Philips) germicidal lamp. The 143 temperature was constant at 18 ± 1 °C (i.e. ambient temperature), during each experimental 144 145 run, since in the shellfish processing industry the washing process takes place at ambient conditions. The exterior reaction vessel was covered with aluminium foil to reflect back UV 146 irradiation. Representative experiments were carried out in triplicates to check the 147 reproducibility of the process. At specific time intervals, 2 mL of the reaction solution were 148 withdrawn and immediately analysed with respect to viable E. coli cells, by the serial dilution 149 150 culture method.

151

152 Schematic 1

153

154 **2.4. Microbiological and chemical analyses**

The detection and quantification of *E. coli* in the processing water was performed using the 155 serial dilution pour plate agar technique. Serial dilutions of the reaction solution were 156 performed in sterile 0.8% (w/v%) NaCl (Fisher Scientific, UK) aqueous solution and 200 µL 157 of each dilution (including neat sample) were pipetted and spread onto Brilliance E. 158 *coli*/Coliform Agar (Oxoid) plates, a selective culture medium. The plates were incubated at 159 37 °C for 20-24 h before viable counts were determined. E. coli colonies appeared with 160 purple colour, while coliforms colonies had a pinkish colour. For the undiluted samples, 1 161 mL of sample was spread over five 90 mm Petri dishes (i.e. 200 µL of sample per Petri dish). 162 This was done to reduce the detection limit to 1 CFU mL⁻¹ for the undiluted samples 163 (Paleologou et al., 2007; Rincón and Pulgarin, 2004). 164

165 The turbidity was measured on a HACH 2100N turbidity meter, while conductivity and pH 166 were measured by a portable conductivity and pH meter (\pm 0.1 pH accuracy), respectively, by 167 Hanna Instruments.

168

169 **2.5. Photoreactivation experiments**

170 Bacteria are known to be capable of repairing their damaged DNA after UV treatment, either by dark repair or by photoreactivation mechanisms (Chatzisymeon et al., 2011; Venieri et al., 171 2011). The latter is considered to be the most important mechanism (Nebot Sanz et al., 2007). 172 In addition, in the seafood processing industry, under study, the tanks, where the shellfish 173 washing water is collected and it is then recycled into the washing process, are open and 174 exposed to natural light. Therefore, in this case, the investigation of bacterial 175 photoreactivation is of major importance. Most photoreactivation studies involve the use of 176 visible light from artificial sources, such as fluorescent lamps, which emit light at 360 nm and 177 halogen lamps emitting between 400 nm and 800 nm. However, very few have dealt with 178 natural light (Chatzisymeon et al., 2011; Vélez-Colmenares et al., 2012; Venieri et al., 2011), 179 as is the case of the present work. Specifically, E. coli photoreactivation experiments in UV 180 treated shellfish washing water were carried out under natural light. For this reason, 100 mL 181 of the final treated effluent were transferred into a sterile conical flask, which was then sealed 182 up to prevent air getting in and potentially contaminating the effluent. The flasks were kept 183 under continuous stirring for about a day (22 h) and under natural light conditions. After this 184 period the final sample was analysed in terms of *E. coli* viability. 185

187 **3. Results and Discussion**

188 **3.1.** Physicochemical and microbiological characteristics of the shellfish washing water

The physicochemical and microbiological characteristics of the collected washing water are 189 190 shown in Table 1, where it can be observed that conductivity is increasing with washing time, from the initial value of 0.05 to 0.52 mS/cm, after 40 min of shellfish washing. This increase 191 in conductivity can be attributed mainly to the increased water salinity, deriving from 192 dissolved salts coming out from shellfish washing. Interestingly, turbidity is increased from 193 0.079 to 42.7 NTU during the first 10 min of washing; while further washing (i.e. from 10 194 min to 40 min) does not considerably affect turbidity. This sharp increase of turbidity from 195 the first 10 min of washing is attributed to solid particles that are washed out from the 196 shellfish; these may include cracked shells, seaweed residuals, etc.. Moreover, turbidity 197 values remained at the same order of magnitude for the rest of the washing time, e.g. 42.7 198 NTU at 10 min to 52 NTU at 40 min. Although, it was expected that water turbidity would be 199 200 rapidly increased, due to the high loads of solids, which are washed out during the washing process, this is not the case here. This can be attributed to the fact that a sieve to hold all large 201 solid particles coming out of the washing process was installed at the end of the shellfish 202 203 washing line, and therefore this is the main reason that turbidity is increased up to a value of about 42 - 52 NTU and after that it remains almost constant with time. Finally, a slight 204 205 increase of pH values by time is also observed, which can be attributed to the increase of conductivity and turbidity. Conductivity (i.e. content of salts in water) and turbidity (i.e. 206 207 suspended solids coming from cracked shells and residual seaweeds) can have neutral or 208 alkaline pH values, thus slightly increasing the pH of the washing water from 5.76 to 6.14.

209

210 Table 1.

211

As far as the microbiological characteristics are concerned, it was observed (Table 1) that pathogen microorganisms, namely *E. coli* along with other coliforms, were increased up to the order of 10^3 and 10^4 CFU mL⁻¹, respectively, after 20 min of washing. Surprisingly, further processing did not cause any greater increase of bacterial concentration in the washing 216 water. This can be explained by the increased (≥ 0.42 mS/cm) conductivity (i.e. salinity) of the water, which prevented the further growth of bacteria in water (Kaspar and Tamplin, 217 1993). In general, enteric bacteria, when released into saline water, are subjected to an 218 immediate osmotic shock, and their ability to overcome this by means of several 219 220 osmoregulatory systems could largely influence their subsequent survival in the marine environment (Rozen and Belkin, 2001). Specifically, the survival of E. coli bacteria in saline 221 water depends, at least partly, on whether they possess certain genes which enable them to 222 regulate osmotic pressure and whether they can be stimulated to express those genes before 223 224 or after their release into the saline aquatic environment (Munro et al., 1989). For example, in a previous study it was observed that survival of E. coli in seawater/distilled water mixtures 225 at different ratios (0, 25, 50, 75 and 100% seawater) for 48 h showed an optimal survival 226 (74%) at the 25% seawater mixture (Carlucci and Pramer, 1960). Moreover, Anderson et al. 227 (1979) who studied the survival of an E. coli isolate for 8 days in seawater at selected 228 salinities (1, 1.5, 2.5, and 3%), observed that decreasing salinity was accompanied by 229 increasing survival (Anderson et al., 1979). Finally, the slight decrease in bacteria counts 230 (Table 1) from 30 min to 40 min of washing can be assumed as negligible, since this is within 231 the same logarithmic order of magnitude. 232

233

3.2. Effect of UV power

235 The effect of UV power on inactivation of bacteria was also studied. For this purpose, three UV lamps, with different power outputs of 5 W, 9 W, and 11W, were used. It should be noted 236 that, in this case, turbidity can be assumed as constant, since there is a similar effect on 237 disinfection efficiency when turbidity values are \geq 42 NTU (see section 3.4). Results are 238 shown in Figure 1, where it is observed that the inactivation of bacteria is rapidly increasing 239 with increasing the power output. Thus, the 11 W UV lamp achieved total inactivation of 240 bacteria after 30 sec of treatment, which was not the case for either the 5 W or the 9 W lamp. 241 Specifically, when initial bacterial concentrations of the order of 10^6 CFU mL⁻¹ are 242 concerned, the 5 W and 9 W germicidal lamps did not achieve water disinfection, not even 243 after 4 min of treatment. In general, photolysis in real water samples occurs directly through 244 light absorption by the organic molecules of the bacterial cells (Chatzisymeon et al., 2011; 245 Nebot Sanz et al., 2007; Vélez-Colmenares et al., 2012; Venieri et al., 2013). Therefore, the 246 higher performance of the 11 W UV system can be attributed to the higher photon flux that 247

248 finally reaches the reactant solution and causes the rapid photolytic degradation of bacteria. In addition, the treatment time obtained here is comparable with previous studies, where E. 249 coli inactivation in biologically treated municipal effluents occurred after 3 min of UV 250 irradiation with an 11 W germicidal lamp (Chatzisymeon et al., 2011). It should be noted that 251 experiments were performed with initial bacterial concentration of 10⁶ CFU mL⁻¹, which is 252 above the real bacterial concentration (i.e. 10⁴ CFU mL⁻¹), as shown in Table 1. This was 253 done to ensure that UV treatment can work under stressed (high bacterial load) conditions. 254 Summing up, a UV germicidal lamp with power output ≥ 11 W can become a feasible option 255 for disinfecting shellfish processing washing waters, thus improving the overall sustainability 256 of the industrial process. 257

258

259 Figure 1.

260

261 **3.3. Effect of bacterial concentration**

The effect of bacterial initial concentration on process efficiency was investigated and the 262 results are presented in Figure 2. Three different initial bacterial concentrations, i.e. 10^4 , 10^5 , 263 and 10^6 CFU mL⁻¹, were tested; which are substantially above the *E. coli* loadings (i.e. $10^3 -$ 264 10⁴ CFU mL⁻¹ as shown in Table 1) in real washing waters. It was observed that inactivation 265 of bacteria occurs more rapidly when their initial concentration is lower. For example, when 266 the initial *E. coli* concentration was 10⁴ CFU mL⁻¹, water was disinfected after 240 sec of 267 treatment, while for initial concentration of 10⁶ CFU mL⁻¹, a substantial amount of *E. coli* 268 (10³ CFU mL⁻¹) survived after 240 sec of treatment. Results in Figure 2 show that the amount 269 of photons emitted from the 9 W germicidal lamp were not adequate to disinfect E. coli of 270 10⁵ and 10⁶ CFU mL⁻¹ initial concentrations, within the first 240 sec of treatment. On the 271 other hand, for initial bacterial concentrations of $\leq 10^4$ CFU mL⁻¹, results show that the 9 W 272 germicidal lamp can be a feasible and applicable option for shellfish processing water 273 disinfection and recycling. Nonetheless, since initial bacterial concentrations are not always 274 $\leq 10^4$ CFU mL⁻¹, disinfection cannot at all times be secured in shellfish processing water, and 275 therefore a germicidal lamp of 11 W, or higher, is proposed as a feasible alternative for 276 recycling shellfish washing water. 277

279 Figure 2.

280

281 **3.4. Effect of water turbidity**

Water turbidity is a parameter that can negatively affect the efficiency of UV treatment, and 282 283 thus its investigation is of major importance. Process efficiency may be inhibited by the presence of suspended solids in the water (Gullian et al., 2012). Inhibition is mainly 284 attributed to the facts that (a) turbidity prevents light from penetrating the whole water 285 matrix, and (b) bacteria can be shielded by solids, thus protecting them from exposure to UV 286 light and therefore preventing their inactivation. Therefore, a series of experiments was 287 performed to assess the effect of water turbidity on process efficiency. The range of turbidity 288 that was examined corresponds to the ones observed in the real shellfish washing water, i.e. 289 35 - 52 NTU, and the results are shown in Figure 3. It can be observed that for turbidity 290 lower than 35 NTU, bacteria are rapidly inactivated after the first 15 sec of treatment. When 291 turbidity values are 42.7 NTU and 52 NTU, results show that E. coli appear to have been 292 inactivated during the first 2 min of UV treatment. However, there is a bacterial increase to 293 15 CFU mL⁻¹ after 4 minutes of treatment and this reappearance can be explained by the fact 294 that the high turbidity of the water (i.e. 42.7 and 52 NTU) can both shield bacteria and hinder 295 296 the penetration of UV irradiation into the whole liquid volume, thus preventing its effective disinfection. Therefore, it is highly recommended that turbidity should be decreased (≤ 35 297 298 NTU) before UV treatment, as to optimize the treatment time and process efficiency.

299

301

302 3.5. Effect of bacterial strain

All the aforementioned experimental series were carried out by spiking *E. coli*, initially isolated from the fresh shellfish washing water, into the same matrix, as to obtain the desirable initial bacterial concentration. In order to confirm and generalize the feasibility of the UV treatment for disinfecting such type of waters, experiments were also performed by using the standard *E. coli* strain ATCC 23716. Results are shown in Figure 4, where it is evident that the disinfection efficiency of the standard strain is slightly higher, than in the

³⁰⁰ Figure 3.

309 case of the bacteria isolated from the real environmental samples. This indicates that isolated bacteria are more persistent to UV treatment than standard strains, thus highlighting the 310 importance of this work which deals with the inactivation of isolated bacteria in real 311 industrial shellfish washing waters. There can be many causes for the difference in the 312 resistance of *E. coli* bacteria to UV treatment. Firstly, during evolution these are possibly 313 exposed to various kinds of environmental stresses, such as temperature, water medium, UV 314 irradiation or chemical agents. Each of these stresses can act differently on the bacterial cell 315 and cause lethality that can vary from strain to strain (Chintagari et al., 2015). Moreover, UV 316 317 is absorbed by nucleic acids producing several types of damage that interfere with replication and transcription of DNA. If UV-induced damage is not repaired or eliminated from DNA, it 318 may lead to mutagenesis and cell death. Mutations not only promote genetic divergence of 319 populations living in different environments, but even in identical environments parallel 320 populations may diverge, if they find alternative adaptive solutions. To prevent the lethal 321 effects of this and other DNA damaging agents, different repair mechanisms have developed 322 through evolutionary history. Therefore, during adaptation of E. coli to UV irradiation, 323 mutations induced in DNA repair or replication genes can be indiscriminately selected 324 (Alcántara-Díaz et al., 2004; Chintagari et al., 2015). 325

326

327 Figure 4.

328

329 **3.6.** Photoreactivation of bacteria

Bacterial photoreactivation experiments were carried out, as to determine the efficiency of 330 UV treatment. At the premises of the seafood processing industry under study, shellfish 331 washing water is exposed to visible light before its further use. Thus the investigation of 332 333 bacterial photoreactivation is imperative in order to ensure the safe UV treated water recycling supply. The results are shown in Table 2 and it is shown that in all cases E. coli 334 photoreactivation occurs after 22 h of exposure to natural light. However, no reactivation was 335 recorded after exposure to light for 2 h, at low initial bacterial concentration (i.e. 10^4 CFU 336 mL⁻¹) (Run 1, Table 2), at low turbidity value of 35 NTU (Run 5, Table 2), and during the 337 treatment of standard E. coli strains (Run 7, Table 2). Therefore, these results indicate that 338 339 UV-C irradiation can cause severe damage to bacterial cells. Comparing the effect of initial

340 bacterial concentration on photoreactivation (Runs 1 - 3), it is observed that in cases where the initial E. coli concentrations are high, i.e. 10⁵ CFU mL⁻¹ and 10⁶ CFU mL⁻¹, 341 photoreactivation takes place after only 2 h of exposure to natural light. This shows that when 342 increasing the initial bacterial concentration at 10⁵ CFU mL⁻¹ and above, photoreactivation is 343 favoured. It should be noted that, in this case, turbidity can be assumed as constant, since as it 344 was proved in section 3.4 there is a similar effect on disinfection efficiency, when turbidity 345 values are \geq 42 NTU. Moreover, as shown in runs 3, 4, and 6, photoreactivation is not 346 affected by the different UV doses and occurs at all UV power outputs (11, 9, and 5 W). This 347 348 is in contrast with previous studies, where it was observed that an increase in UV dose is valuable in minimizing photoreactivation events, since reduced UV dose causes reduced 349 DNA damages on targeted bacteria, thus increasing the risk of subsequent photoreactivation 350 (Lindenauer and Darby, 1994; Nebot Sanz et al., 2007). However, in this case it should be 351 noted that runs 3, 4, and 6 are carried out at high turbidity values (i.e. 42 - 52 NTU) that has 352 been proved to decrease disinfection efficiency. Not only this but, if runs 5 and 6 are 353 compared, it is observed that at low turbidity values (i.e. 35 NTU) photoreactivation of 354 bacteria does not occur for at least 2 h after UV treatment, while when turbidity is 52 NTU 355 (run 6) photoreactivation takes place within the first 2 h after UV treatment. Furthermore, 356 from runs 5 and 7, it can be concluded that bacterial strain has an effect on photoreactivation 357 of E. coli, since, although both strains were reactivated after 22 hours of exposure, the cell 358 359 count was higher for isolated bacteria. This is consistent with the results described in Figure 4 and enhances the fact that isolated bacteria are more resistant to UV treatment than standard 360 361 strains, such as the ATCC 23716, which also highlights the significance of this work.

362

363 Table 2.

364

365 4. Conclusions

In this work the feasibility of UV treatment to disinfect shellfish processing water was assessed. For this purpose, the effect of important operating parameters, such as the initial bacterial concentration, UV power output, water turbidity and treatment time, on process efficiency was investigated. It should be noted that although this is a pressing problem for seafood industry, it has received very little attention till now. The main findings of this workcan be summarized as follows:

372 - Shellfish washing waters are turbid and saline with values ranging between 35 - 52 NTU

and 0.28 - 0.52 mS/cm, respectively. Regarding their microbiological characteristics, there

is a built-up of *E. coli* and other coliforms of the order of 10^3 CFU ml⁻¹ and 10^4 CFU mL⁻¹,

- 375 respectively.
- UV treatment can be efficiently applied to disinfect shellfish washing water, since it was observed that, at optimal operating conditions (i.e. UV power output at 11 W, water turbidity \leq 35 NTU and initial *E. coli* concentration up to 10⁶ CFU mL⁻¹) the total inactivation of bacteria is achieved after only 15 sec of treatment.
- Bacterial photoreactivation experiments were carried out and showed that no *E. coli* photoreactivation occurs, after exposure to light for 2 h, at low initial bacterial concentration (i.e. 10^4 CFU mL⁻¹), at low turbidity value of 35 NTU, and during the treatment of standard *E. coli*. Hence, it can be concluded that UV disinfection of shellfish washing waters, with initial bacterial loading of up to 10^4 CFU mL⁻¹, can be a very efficient treatment process in the presence of a UV lamp with power output of 11 W and when turbidity of the washing water is decreased to ≤ 35 NTU.
- 387

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390

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488 List of Schematics

- 490 Schematic 1. Experimental set up of the UV reactor. Compartments: (1) exterior cylindrical
- 491 reaction vessel made of borosilicate glass, and (2) inner quartz glass tube housing the lamp.



492

496 Schematic 1. Experimental set up of the UV reactor. Compartments: (1) exterior cylindrical

497 reaction vessel made of borosilicate glass, and (2) inner quartz glass tube housing of the

498 lamp.

499 List of Tables

500

Table 1. Physicochemical and microbiological characteristics of shellfish washing watersamples. The standard deviation (SD) is shown in brackets.

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Table 2. *E. coli* photoreactivation, under natural light, in UV treated shellfish processing
water.

Table 1. Physicochemical and microbiological characteristics of shellfish washing watersamples. The standard deviation (SD) is shown in brackets.

Characteristics	Sample (shellfish washing time)						
Characteristics	1 (0 min)	2 (10min)	3 (20 min)	4 (30 min)	5 (40 min)		
Conductivity, mS/cm	0.05	0.28	0.42	0.46	0.52		
рН	5.76	5.87	5.98	6.2	6.14		
Turbidity, NTU	0.079	42.7	42	35	52		
<i>Escherichia coli</i> , CFU mL ⁻¹	0 (SD=0)	510 (SD=14)	1235 (SD=230)	7530 (SD=1010)	2420 (SD=380)		
Coliforms, CFU mL ⁻¹	0	750	20000	33583	15375		

512 Table 2. *E. coli* photoreactivation, under natural light, in UV treated shellfish processing 513 water.

Operating conditions of UV treatment				E. coli			
Run	Lamp power, W	Turbidity, NTU	Initial <i>E. coli</i> concentration , CFU mL ⁻¹	Bacterial strain	survival after 240 sec of UV treatment, CFU mL ⁻¹	<i>E. coli</i> survival after 2h of phototreatment , CFU mL ⁻¹	<i>E. coli</i> survival after 22h of phototreatment, CFU mL ⁻¹
1	9	52	10 ⁴	Isolated	0	0	100
2	9	52	10 ⁵	Isolated	57	18	>100
3	9	42	10 ⁶	Isolated	2600	>100	>100
4	5	42	10 ⁶	Isolated	7500	>100	>100
5	11	35	10 ⁶	Isolated	0	0	>100
6	11	52	10 ⁶	Isolated	15	>100	>100
7	11	35	10 ⁶	ATCC23716	0	0	20

516 List of Figures

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- Figure 1. Inactivation of bacteria under different UV power outputs. Conditions: Initial bacterial concentration = 10^6 CFU mL⁻¹; water turbidity = 42 52 NTU.
- 520 Figure 2. Inactivation of bacteria under different initial bacterial concentrations. Conditions:
- 521 UV power = 9 W; water turbidity = 52 NTU.
- 522 Figure 3. Inactivation of bacteria under different water turbidity values. Conditions: UV
- 523 power = 11 W; initial bacterial concentration = 10^6 CFU mL⁻¹.
- 524 Figure 4. Inactivation of bacteria in the presence of different *E. coli* strains. Conditions: UV
- power= 11 W; initial bacterial concentration = 10^6 CFU mL⁻¹; water turbidity = 35 NTU.

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Figure 1. Inactivation of bacteria under different UV power outputs. Conditions: Initial bacterial concentration = 10^6 CFU mL⁻¹; water turbidity = 42 - 52 NTU.



Figure 2. Inactivation of bacteria under different initial bacterial concentrations. Conditions:
UV power = 9 W; water turbidity = 52 NTU.



Figure 3. Inactivation of bacteria under different water turbidity values. Conditions: UV power = 11 W; initial bacterial concentration = 10^6 CFU mL⁻¹.



544 Figure 4. Inactivation of bacteria in the presence of different *E. coli* strains. Conditions: UV

power= 11 W; initial bacterial concentration = 10^6 CFU mL⁻¹; water turbidity = 35 NTU.