

## FULL PAPER

# Selective Primary Alcohol Oxidation of Lignin Streams from Butanol-Pretreated Agricultural Waste Biomass

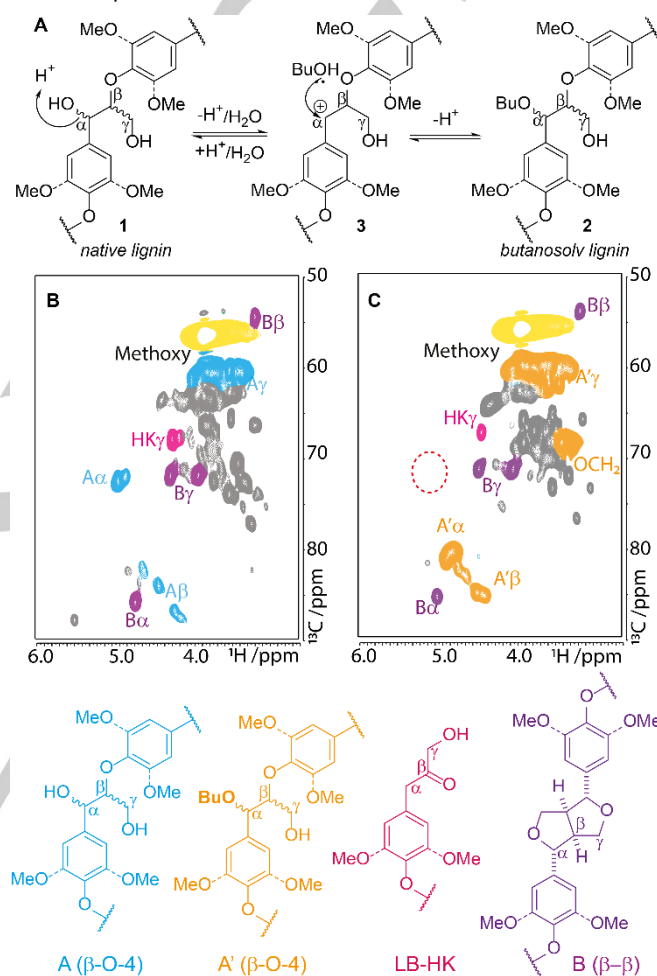
Isabella Panovic,<sup>[a]</sup> Christopher S. Lancefield,<sup>[a]</sup> Darren Phillips,<sup>[b]</sup> Mark J. Gronnow,<sup>[b]</sup> and Nicholas J. Westwood\*<sup>[a]</sup>

**Abstract:** Chemically modified lignins are important for the generation of biomass-derived materials and as precursors to renewable aromatic monomers. A butanol-based organosolv pretreatment has been used to convert an abundant agricultural waste product, rice husks, into a cellulose pulp and three additional product streams. One of these streams, a butanol-modified lignin, was oxidised at the  $\gamma$ -position to give a carboxylic acid functionalized material. Subsequent coupling of the acid with aniline aided lignin characterization and served as an example of the flexibility of this approach for grafting side chains onto a lignin core structure. The pretreatment was scaled up for use on a multi-kilogram scale, a development that enabled the isolation of an anomeric mixture of butoxylated xylose in high purity. The robust and scalable butanosolv pretreatment has been developed further and demonstrates considerable potential for the processing of rice husks.

## Introduction

Lignocellulosic biomass consists of a mixture of cellulose (c.a. 30–50%), lignin (c.a. 10–30%) and hemicellulose (c.a. 20–35%).<sup>[1]</sup> Currently, the Kraft and liginosulfonate processes deliver large quantities<sup>[2,3]</sup> of valuable saccharide product streams at the required high purity levels. These methods also give a lignin stream which is typically burnt on-site to return energy back into the process or is used in low value materials as an additive or binding agent.<sup>[4]</sup> There is considerable interest in higher value uses for lignin, due to its aromatic-rich structure, with research dominated by two main approaches: (i) its use in polymeric materials for co-polymer blending and grafting applications,<sup>[5,6]</sup> and (ii) its depolymerisation to useful aromatic monomers.<sup>[7–9]</sup> The structural complexity of lignin offers both a challenge and an opportunity. In theory a wide range of different feedstock

chemicals and functional materials could be generated from lignin if suitable processes can be found.



**Figure 1.** A Comparison of dioxasolv and butanosolv lignins. **A** Mechanism of formation of butoxylated  $\beta$ -O-4 units during the butanosolv process. In an acidic organosolv pretreatment, benzylic cation **3** is formed from native  $\beta$ -O-4 unit **1**. For butanosolv, **3** is converted to a butoxylated  $\beta$ -O-4 unit **2**. In contrast for dioxasolv, **3** reacts to form condensed C-C bond containing units and lignin-bound Hibbert's ketones (LB-HK).<sup>[10]</sup> **B** and **C** 2D HSQC NMR (700 MHz,  $d_6$ -DMSO) analysis of **B** dioxasolv walnut shell lignin and **C** butanosolv walnut shell lignin. Full conversion to the butoxylated  $\beta$ -O-4 unit **3** (orange signals) often occurs in the butanosolv process, as shown by the complete loss of the cross-peaks (highlighted in dashed red circle) corresponding to the native  $\beta$ -O-4 unit **1** (blue signals).

[a] Miss I. Panovic, Dr. C. S. Lancefield, Dr N. J. Westwood\*  
School of Chemistry & Biomedical Sciences Research Complex,  
University of St Andrews and EaStCHEM,  
North Haugh, St Andrews, Fife (UK) KY16 9ST  
E-mail: [njw3@st-andrews.ac.uk](mailto:njw3@st-andrews.ac.uk)

[b] Mr D. Phillips, Dr M. J. Gronnow  
Biorenewables Development Centre,  
1 Hassacarr Close, Chessingham Park, Dunnington, York (UK)  
YO19 5SN

Supporting information for this article is given via a link at the end of the document.

Most biorefineries focus on the carbohydrate product streams, meaning severe conditions are used to remove the "contaminating" lignin. Typically the lignin's  $\beta$ -O-4 unit (structure

1 in Figure 1A), which is the most abundant unit in native lignins, is heavily degraded. Destruction of the  $\beta$ -O-4 unit and extensive formation of additional C-C bonds (condensation) yields lignins that are less chemically tractable than the native biopolymer.<sup>[11,12]</sup> In contrast, some organosolv pretreatments treat lignocellulosic biomass<sup>[13,14]</sup> more gently with the drawback that less pure carbohydrate streams are formed. In addition, due to the frequent use of acidic conditions, some organosolv lignins are still condensed. We<sup>[15]</sup> and others<sup>[16–20]</sup> have previously reported the use of biorenewable butanol as a pretreatment solvent for woody-biomass sources, using both hardwoods and softwoods.<sup>[15]</sup> Under the acidic butanosolv conditions, the hydroxyl at the  $\alpha$ -position of the  $\beta$ -O-4 unit is replaced by butanol leading to stabilisation of the  $\beta$ -O-4 unit in a “protected”<sup>[21]</sup> form (structure 2, Figures 1 and S1). Failure to trap benzylic cations such as 3 results in condensation or the formation of (lignin-bound) Hibbert’s ketones (LB-HK, Figure 1).<sup>[10]</sup> Another example of a “protected lignin” was reported recently by Luterbacher *et al.* who created a aldehyde-stabilised lignin in which the  $\beta$ -O-4  $\alpha$ - and  $\gamma$ -hydroxyls were tethered together (double protection).<sup>[22,23]</sup>

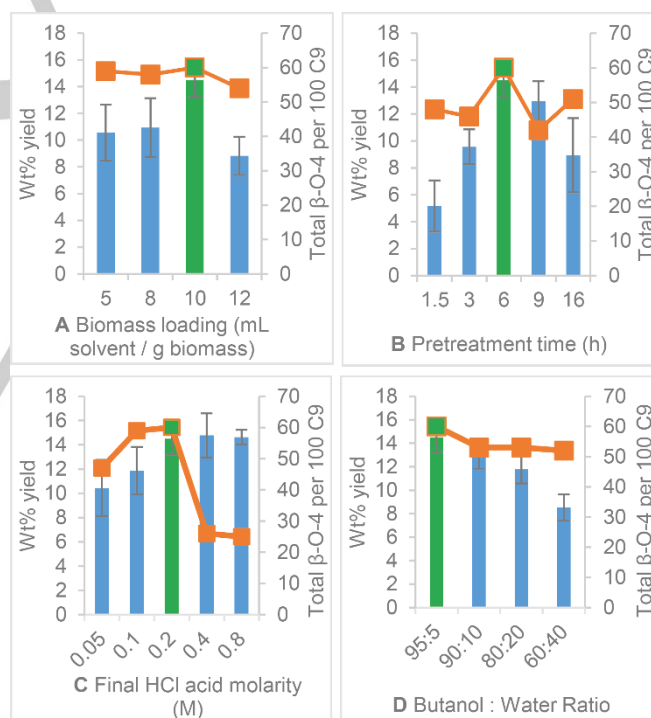
In agriculture the majority of crops produced come from herbaceous monocots, such as rice, wheat, sugarcane and maize, and therefore large volumes of agricultural waste from these sources are generated annually. Among these, rice is one of the most cultivated crops in the world with around 680 million tonnes produced per annum.<sup>[24]</sup> Rice husks make up around 20 wt% of the rice grain and are composed of approximately 22% lignin, 38% cellulose, 18% hemicelluloses, 2% extractives and 20% ashes with variations depending on geographical origin.<sup>[25,26]</sup> As a result of high lignin and ash content, the husks are not a viable animal feed,<sup>[27]</sup> but they can be burnt to yield large quantities of silica that can be used in a number of material applications.<sup>[25,27–33]</sup> However, compared to the relatively well valorised polysaccharide fractions and processing of rice husk-derived silica, little attention has been paid to the abundant lignin fraction.

Here, we report that a butanol-based organosolv pretreatment of rice husks allows for efficient processing of the biomass. We show that this process is scalable up to a multi-kilogram scale and that the resulting rice husk butanosolv lignin (RHBL) has high  $\beta$ -O-4 content with the expected incorporation of butanol at the  $\alpha$ -position of the  $\beta$ -O-4 unit. RHBL is shown to be a suitable substrate in an organocatalytic oxidation to give a  $\gamma$ -carboxylic acid-containing lignin that can be used in amide

coupling reactions. Butoxylated xylose (mixture of anomers) is also isolated in high purity from a hemicellulose-derived stream.

## Results and Discussion

Previously we have described the application of butanosolv pretreatment of beech (hardwood), walnut shells (hardwood endocarp) and Douglas fir (softwood) (Table S1, entries 1-3, Figure S4).<sup>[15]</sup> In each case the cellulose was retained in a pulp and a soluble fraction containing modified hemicellulose monosaccharides and lignin was removed by filtration (Figure S2). Here, the initial goal was to optimise the butanosolv pretreatment for use with a herbaceous monocot agricultural waste product (Figure S3).<sup>[34]</sup> The aim was to determine mild conditions capable of delivering rice husk butanosolv lignin (RHBL) in optimal yields with high retention of  $\beta$ -O-4 content ( $\beta$ -O-4 per 100 C9 unit calculation, Figure S5 and Table S2).



**Figure 2.** Graphs showing lignin weight % yields (bar charts) and total  $\beta$ -O-4 per 100 C9 data (line chart); **A** Effect of changing biomass loading (conditions identical except for quantity of solvent system used per gram of rice husks); **B** Pretreatment time (time pretreatment was maintained at reflux); **C** Final hydrochloric acid molarity in 95:5 butanol/water solvent system; **D** Ratio of butanol to water using a fixed final concentration of 0.2 M HCl. The optimal conditions based on both lignin wt% yields (green bars) and  $\beta$ -O-4 per 100 C9 values are shown. All pretreatments were performed on a 4 g scale. Error bars are based on three repeats of each pretreatment.

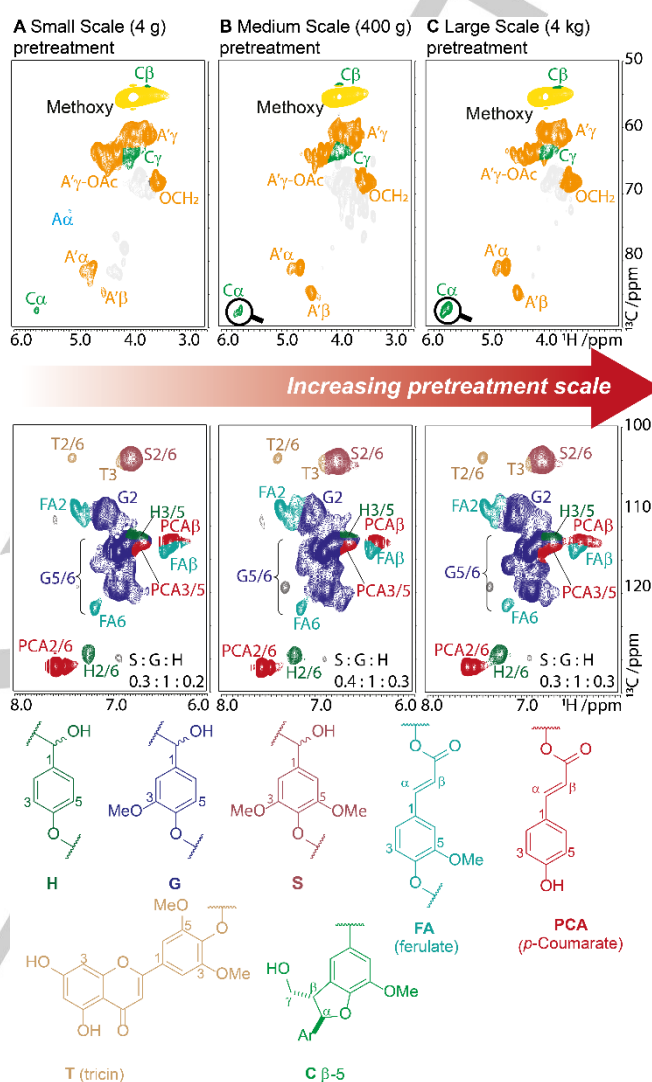
A range of biomass loadings were initially assessed varying from 5-12 mL of solvent per gram of rice husks. Whilst all the loadings led to the isolation of RHBL with a high total  $\beta$ -O-4 content, the lignin yield was optimal at 10 mL/g (Figure 2A). Using this loading level, it was then shown that the reflux time also affected the lignin yield. The optimal outcome was obtained after 6 hours at reflux with yields dropping at extended times, presumably due to lignin condensation resulting in a significant proportion of the lignin being in the insoluble pulp (Figure 2B). Upon varying the acid molarity whilst retaining a butanol:water ratio of 95:5 (using 10 mL/g loading and 6 hours at reflux), the highest yield of high quality RHBL was obtained when a final concentration of acid of 0.2 M was used. A significant decrease in the  $\beta$ -O-4 content was observed when higher concentrations of acid were used (Figure 2C) as expected.<sup>[13]</sup> Finally, when the final acid concentration was fixed at 0.2 M, varying the butanol:water ratio showed that with increasing amounts of water relative to butanol, there was a decrease in yield (Figure 2D). Optimal conditions for the butanosolv pretreatment of rice husks were determined to be: biomass loading of 10 mL/g, 6 h pretreatment time, 0.2 M final concentration of hydrochloric acid in a 95:5 butanol:water ratio.

Gel permeation chromatography (GPC) analysis of RHBL was conducted during the optimisation study (Table S2). A general decrease in  $M_w$  was observed with an increase in final acid molarity ( $M_w$  3939 for 0.05 M *c.f.*  $M_w$  2842 for 0.8 M) consistent with more acidic conditions leading to increased lignin cleavage and a reduction in chain length.

The scalability of the process was studied next. The quality of the RHBL was very similar over a pretreatment scale that ranged from 4 g to 400 g to 4000 g. This was assessed using 2D HSQC NMR analysis and semi-quantitative integration of the spectra obtained for the different batches of RHBL (Figure 3, Table S3 and Figure S6). Yields of the different product streams were also reproducible across all the scales tested (Table S3).

The separation of the RHB lignin and the hemicellulose-derived (RHBH) streams using our published work-up protocol<sup>[15]</sup> proved challenging on larger scale (Figures S1 and S7A-E). The use of the contrasting solubility of the lignin (insoluble) and the hemicellulose-derived streams (soluble) in aqueous solution was effective for small-scale pretreatments (Figure S7B) and small portions (28 g) of the crude hemicellulose-derived/lignin mixture retained from larger pretreatments (Figure S7C). However, attempts to process all the material from a 400 g pretreatment

were hampered by very long filtration times after lignin precipitation (Figure S7D). The requirement to use large quantities of water for the lignin precipitation also meant that



**Figure 3.** Sidechain and aromatic regions of 2D HSQC NMR spectra (700 MHz,  $d_6$ -Acetone) of extracted RHBL at different scales; **A** Small scale pretreatment (4 g rice husks); **B** Medium scale (400 g rice husks); **C** Large scale (4 kg rice husks). Colour palette used for different linkages, with the rest of the colour palette shown with Scheme 1. Magnification shown is x2 intensity.

obtaining the RHBH was tiresome (Figure S7D & S7E). A modified work-up protocol was developed for large scale work (Figure S7A) in which the aqueous solution of the RHBH was first extracted with EtOAc giving separate water- and EtOAc-soluble RHBH streams. In one run, this led to 34% of the RHBH being in the EtOAc layer with the remainder being in the water. Furthermore, extended filtration times were avoided by centrifugation.

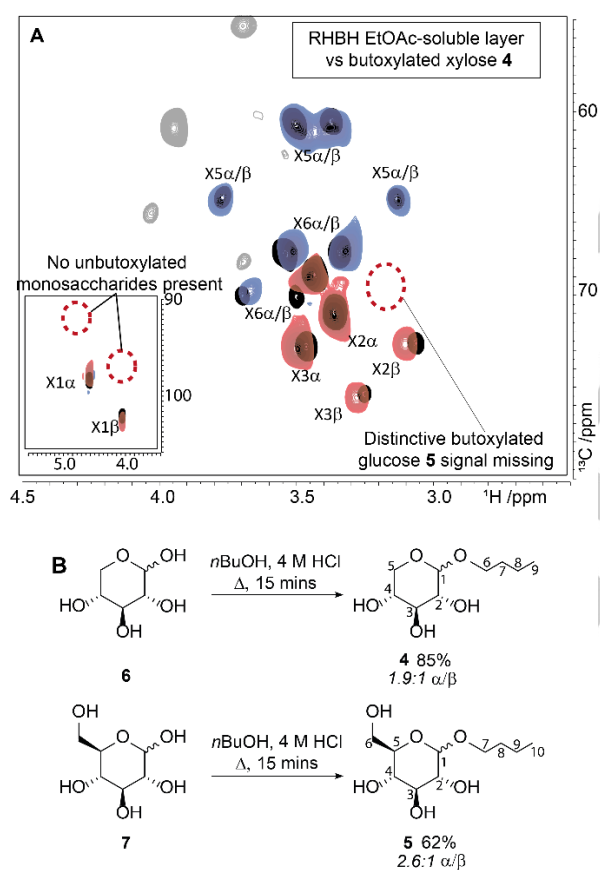
In previous work with hardwood butanosolv lignins<sup>[15]</sup> it was demonstrated that hemicellulose was depolymerised and chemically modified by butoxylation at the anomeric position of the monomeric sugars. In this work, the presence of specific sugar monomers was determined using 2D HSQC NMR analysis with spectra of authentic butoxylated xylose **4**, butoxylated glucose **5** and xylose **6** being used for comparison (Figure 4 and Figure S8A-G). The ethyl acetate-soluble stream was shown to be almost entirely comprised of butoxylated xylose **4** with some minor unknown contaminants (Figure 4). Whereas, the water-soluble stream was comprised of a mixture of native and butoxylated monosaccharides **4-7** (Figure S8) and some minor unidentified components. In an attempt to purify the mixture by flash column chromatography (using a 0-15% MeOH/DCM

system), from 2 g of the crude lignin/hemicellulose mixture, 0.4 g of **4** and 0.2 g of **5** were obtained in excellent purity (Figure S9). Unfortunately, other native monosaccharides proved too polar to be eluted. Based on quantitative HSQC NMR analysis of the crude hemicellulose stream we estimate that the yields of butoxylated xylose **4** and glucose **5** are approximately 16 and 5 wt% respectively, and non-butoxylated xylose **6** <2 wt%, with respect to the starting biomass (Tables S4-S7 and Figures S13-S15). Furthermore, the yield of butoxylated xylose **4** in the EtOAc extract was found to be approximately 4 wt%, again with respect to the starting biomass (Table S7).

### TEMPO-mediated formation of $\beta$ -O-4 $\gamma$ -carboxylic acid-substituted butanosolv lignins

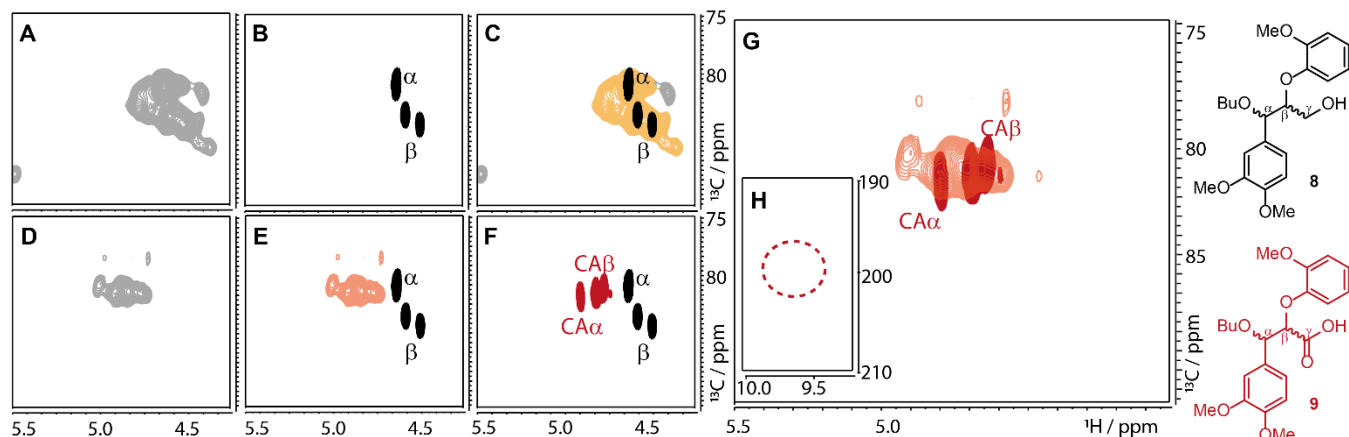
In contrast to other RH product streams,<sup>[35-37]</sup> the lignin has been understudied with the exception of its structural characterisation.<sup>[26,38,39]</sup> It was therefore decided to assess if RHBL could be converted into a precursor for novel materials. Strategies for lignin modification often focus on the use of phenolic end groups and/or the unselective conversion of  $\beta$ -O-4 units by reaction at both the  $\alpha$ - and  $\gamma$ -hydroxyls. In the case of butanosolv lignins, only the  $\beta$ -O-4  $\alpha$ -hydroxyl is substituted,<sup>[8]</sup> providing an opportunity to carry out site selective oxidation of the  $\gamma$ -hydroxyl to the corresponding  $\gamma$ -carboxylic acid (to give lignin <sup>$\gamma$ -oxCA</sup>). It should be noted that a proportion of the  $\beta$ -O-4 units in RHBL are natively  $\gamma$ -acylated with sidechain esters such as *p*-coumarates (Figure S10) and that these  $\gamma$ -Ac- $\beta$ -O-4 units would be inert to the planned oxidation reactions.<sup>[26,38,39]</sup>

Previous reports on  $\beta$ -O-4  $\gamma$ -oxidation have focussed on the generation of aldehydes (lignin <sup>$\gamma$ -oxALD</sup>) in model systems and *en route* to lignin depolymerisation.<sup>[40,41]</sup> To the best of our knowledge, only three reports describe the preparation of model  $\beta$ -O-4  $\gamma$ -carboxylic acids and organosolv lignin <sup>$\gamma$ -oxCA</sup>. All of these use TEMPO as the catalytic oxidant under electrochemical catalyst regeneration conditions.<sup>[42-44]</sup> The initial report focussed on non-phenolic native  $\beta$ -O-4 models<sup>[42]</sup> and showed that the use of alkaline conditions was advantageous. Later, Stahl reported additional studies on the  $\gamma$ -oxidation of phenolic native  $\beta$ -O-4 models and concluded that, whilst cleavage reactions dominated, quinone methide structures were formed under basic conditions with TEMPO.<sup>[43,44]</sup> It seems clear that the presence of phenolic end-groups in lignin may well be problematic for the  $\gamma$ -oxidation of  $\beta$ -O-4 unit. Indeed, Stahl indicated that using lignins with lower native phenolic content resulted in more efficient  $\gamma$ -oxidation.



**Figure 4.** **A** Multiplicity edited 2D HSQC NMR analysis (700 MHz, D<sub>2</sub>O) of EtOAc-soluble hemicellulose stream (blue and pick signals) overlaid with the spectra obtained on analysis of an authentic sample of  $\alpha/\beta$ -butoxylated xylose **4** (black). Multiplicity-edited cross-peaks corresponding to CH<sub>2</sub> proton environments (blue) and multiplicity-edited cross-peaks corresponding to CH proton environments (red) shown. The anomeric region (inset box) highlights the absence of native monosaccharides (dashed regions). The absence of the distinctive G5 $\alpha/\beta$  cross-peak observed in butoxylated glucose **5** is highlighted (dashed regions). **B** Reaction scheme showing preparation of authentic butoxylated monosaccharide standards **4** and **5**.





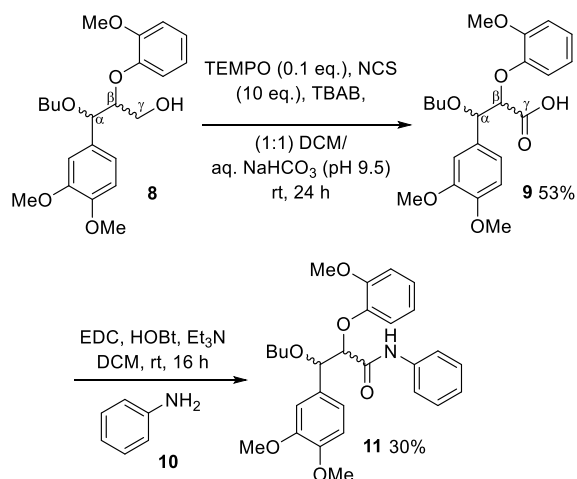
**Figure 5.** HSQC NMR analysis (700 MHz,  $d_6$ -DMSO) of RHBLs; Signals corresponding to a selected region of the analysis of: **A** unmodified RHBL; **B** model **8**; **C** overlay of model **8** and unmodified RHBL; **D** RHBL <sup>$\gamma$ -oxCA</sup> (prepared using general procedure C); **E** overlay of RHBL <sup>$\gamma$ -oxCA</sup> and model **8**; **F** overlay of model **8** (black) and model **9** (red); **G** overlay of RHBL <sup>$\gamma$ -oxCA</sup> and model **9**; **H**  $\delta^1\text{H}/\delta^{13}\text{C}$  9–10 ppm/190–210 ppm region in RHBL <sup>$\gamma$ -oxCA</sup> highlighting the absence of an aldehyde signals (dashed red region). For a full labelled RHBL <sup>$\gamma$ -oxCA</sup> spectrum, refer to Figure S11A.

Despite the fact that lignin from grasses is known to have a high native phenolic content due to coumarates and ferulates, it was decided to attempt to convert our RHBL to RHBL <sup>$\gamma$ -oxCA</sup> using a TEMPO/NCS system that had previously been reported to oxidise relatively simple primary alcohols.<sup>[45]</sup>

Encouragingly, butoxylated  $\beta$ -O-4 model **8** was oxidised allowing isolation of  $\gamma$ -acid model **9** (Schemes 1 and S2). Subsequent formation of the  $\beta$ -O-4  $\gamma$ -carboxylic acid in RHBL was observed when the reaction was run with catalytic quantities of TEMPO at pH 9–10 for extended reaction times (Scheme S1, general procedure C) with a significant excess of NCS being used as a co-oxidant. Noticeable changes in the chemical shift of the cross-peaks corresponding to the butoxylated  $\beta$ -O-4 unit were seen upon  $\gamma$ -oxidation (from  $\delta^1\text{H}/\delta^{13}\text{C}$  4.5 ppm/82 ppm for the  $\alpha$ -proton and 4.4 ppm/83 ppm of the unreacted unit to 4.7 ppm/82 ppm for the  $\alpha$ -proton and 4.6 ppm/81 ppm for the  $\beta$ -proton of the  $\gamma$ -oxidised unit, Figure 5). Evidence for the successful formation of RHBL <sup>$\gamma$ -oxCA</sup> also came from good overlay with signals from the relevant model **9** (Figure 5G) and not the unoxidised model **8** (Figure 5E and 5G). The formation of RHBL <sup>$\gamma$ -oxCA</sup> occurred selectively under these conditions with no detectable formation of RHBL <sup>$\gamma$ -oxALD</sup> (absence of signals corresponding to aldehyde environments in RHBL <sup>$\gamma$ -oxCA</sup>, Figure 5H inset).

Quantitative  $^{31}\text{P}$  NMR analysis was also supportive of a significant increase in carboxylic acid environments in the RHBL <sup>$\gamma$ -oxCA</sup> compared to unoxidised RHBL (Figure S12). However, there was a significant loss of signals corresponding to phenols, potentially consistent with the previously reported quinone methide formation.<sup>[43,44]</sup> The analogous  $\gamma$ -oxidation of other butanosolv lignins was conducted and demonstrated that this approach was generally applicable. Walnut shell butanosolv lignin (WSBL, from a hardwood source, Figure 1 and Figure S4C), buckwheat butanosolv lignin (BWBL, hardwood, Figure S4K) and Douglas fir butanosolv lignin (DFBL, softwood, Figure S4I) were all successfully converted to the corresponding  $\gamma$ -carboxylic acid-containing materials (Figure S11).

With RHBL <sup>$\gamma$ -oxCA</sup> in hand, it was decided to couple the newly introduced carboxylic acids with aniline **10**, as it was felt this represented a flexible approach to grafting onto the lignin backbone that complemented other recent reports by us and others.<sup>[5,46–52]</sup> Initially, model **11** was synthesised from **9** and **10** to aid characterisation of the final lignin (Scheme 1). RHBL <sup>$\gamma$ -oxCA</sup> was then coupled with **10** using EDC, Et<sub>3</sub>N and HOBt at rt for 24 hours (Lignin general procedure D).<sup>[53]</sup> The resulting lignin was characterised using HSQC NMR analysis (Figure 6) and compared with model **11** (Figure 6A). Aniline **10** was selected for these studies as on formation of the lignin-aniline amide bond a distinctive change in the chemical shift of the aniline aromatic protons was expected. Comparison of the signals observed for the  $\gamma$ -coupled lignin with those of aniline **10** and acetylated aniline **12** (and model **11**) supported the formation of the desired amide bond in the lignin (Figures 6A and 6B). As expected, the cross-peaks corresponding to the aromatic protons in aniline **10** ( $\delta^1\text{H}/\delta^{13}\text{C}$  7.0 ppm/129 ppm, 6.5 ppm/116 ppm and 6.6 ppm/114 ppm) were very distinct from the cross-peaks in acetylated aniline



**Scheme 1.** Preparation of butoxylated  $\gamma$ -acid  $\beta$ -O-4 model **9** and EDC/HOBt/Et<sub>3</sub>N amide coupling with aniline **10** to give  $\gamma$ -coupled model **11**.

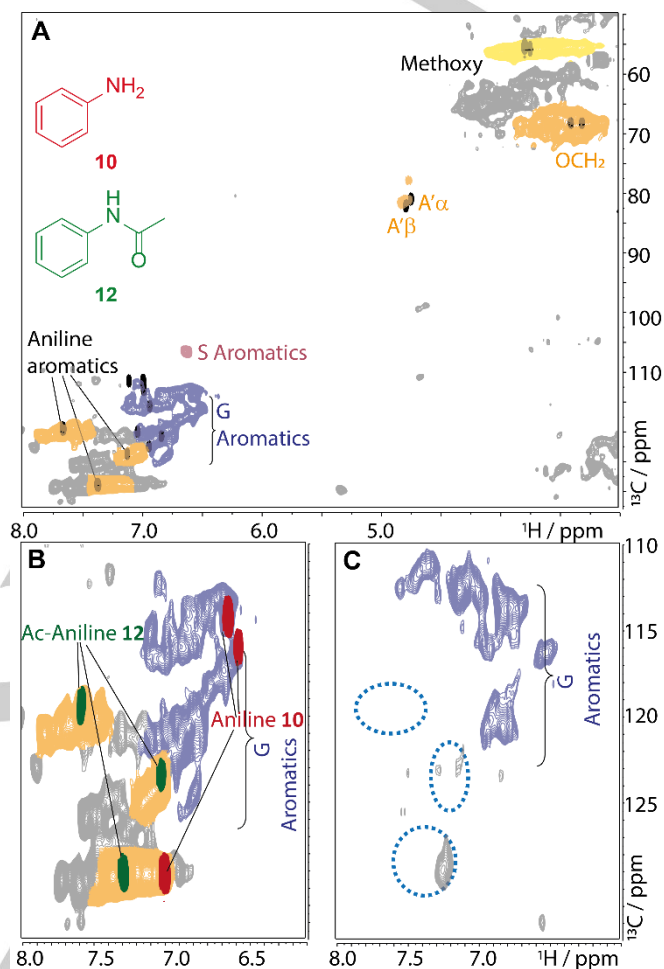
**12** ( $\delta^1\text{H}/^{13}\text{C}$  7.6 ppm/119 ppm, 7.3 ppm/129 ppm and 7.0 ppm/123 ppm), model **11** and in the coupled RHBL <sup>$\gamma$ -amide</sup>. There was a clear appearance of new aniline-related aromatic cross peaks that were not present in the starting RHBL <sup>$\gamma$ -oxCA</sup> (Figure 6C).

## Conclusions

The butanosolv pretreatment process was applied to rice husks with variations in a number of the reaction parameters being carried out. Optimal conditions were determined to be a 10 mL/g solvent to biomass loading, in a 95:5 ratio of butanol to water at a final acid molarity of 0.2 M for a pretreatment time of 6 h at reflux. This process was shown to be efficient on a variety of scales, with repeatably good conversion of biomass into high quality product streams on scales of up to 4 kg of biomass. Pure butoxylated xylose (anomeric mixture) was isolated directly from the pretreatment in high yield based on the amount of xylose present in the starting biomass. In addition, selective  $\gamma$ -oxidation of the butoxylated  $\beta$ -O-4 units in the butanosolv rice husk lignin gave  $\gamma$ -carboxylic acids despite the presence of phenolic end groups in the lignin. Evidence for the success of this selective lignin oxidation protocol came from detailed HSQC and <sup>31</sup>P NMR analysis including comparison with relevant model compounds. However, preparation of RHBL <sup>$\gamma$ -oxCA</sup> required a significant amount of the co-oxidant NCS and the system is relatively complex. Future work will strive to reduce the complexity of the oxidation system.

Finally, the oxidised lignin was used in an exemplar amide coupling reaction leading to an amide-grafted lignin. The potential

for the controlled preparation of a range of complex lignins via this overall approach is considerable.



**Figure 6:** HSQC NMR analysis (700 MHz, d<sub>6</sub>-DMSO) of RHBL <sup>$\gamma$ -amide</sup>. **A** spectrum of  $\gamma$ -coupled RHBL overlaid with spectrum of model **11** (black). Environments corresponding to  $\gamma$ -coupled  $\beta$ -O-4 protons are coloured in orange. **B** aromatic region from analysis of  $\gamma$ -coupled RHBL overlaid with spectra of aniline **10** (red) and acetylated aniline **12** (green). **C** aromatic region from analysis of starting RHBL <sup>$\gamma$ -oxCA</sup> highlighting absence of signals corresponding to aniline aromatic environments are clearly absent (highlighted in blue dashed circles).

## Experimental Section

All chemicals used in this report were obtained from commercial sources. Rice husks biomass was obtained from The Home Brew Shop, walnut shell biomass was a kind donation from Sharpham Park farm, and all other biomasses were received from Hot Smoked. Full characterisation data consisting of <sup>1</sup>H NMR, <sup>13</sup>C NMR, 2D HSQC NMR, IR and HRMS are provided for all novel compounds (refer to ESI).

### Lignin General Procedure A: Butanosolv Pretreatment

Following a literature procedure,<sup>[15]</sup> to unextracted biomass was added *n*-butanol: 0.2 M HCl (95:5, 10 mL/g). The mixture was heated at a gentle reflux (ca. 100 °C) for 6 h and vacuum filtered when cooled. The residual

pulp was washed with a solution of acetone:H<sub>2</sub>O (9:1), and the resultant filtrate was concentrated *in vacuo* to yield a gum-like residue (azeotrope with additional portions of water to remove all butanol). The residual pulp (cellulose-enriched pulp) was dried in a vacuum oven overnight at 50 °C. The gum-like residue was dissolved in the minimum amount of acetone:H<sub>2</sub>O (9:1, 5 mL/g) and added dropwise to rapidly stirring H<sub>2</sub>O (50 mL/g, 10 v/v minimum). A small portion of sat. sodium sulfate solution added (1 mL/100 mL water). The resulting crude precipitate was collected by vacuum filtration, or centrifugation at 8 000 rpm, and dried in a vacuum oven at 50 °C for 16 h.

#### Lignin General Procedure B: Phosphitylation and <sup>31</sup>P NMR analysis of Lignin

All lignins were dried for 16 h at 50 °C in a vacuum oven before measurements. 30 mg of lignin was weighed into a vial and dissolved in 0.5 mL of CDCl<sub>3</sub>/pyridine (1:1.6, anhydrous, dried over 4 Å MS). Following a literature procedure,<sup>[54]</sup> to this solution was added 10 μL cyclohexanol (dried over 4 Å MS) and 50 μL 2-chloro-4,4,5,5-tetramethyl-1,3,2-dioxaphospholane. The solution was transferred to a clean, dry NMR tube, purged with N<sub>2</sub> and sealed, then analysed using quantitative <sup>31</sup>P NMR analysis within 6 h of sample prep.

#### Lignin General Procedure C: TEMPO/NCS γ-Oxidation to Butanosolv Lignin<sup>γ-oxCA</sup>

To a solution of butanosolv lignin (0.4 g) and TBAB (0.03 g) in a DCM/aq. buffered system (1:1, 2 mL, aq. sat. NaHCO<sub>3</sub>, pH 9-10) was added NCS (1 g) and TEMPO (0.12 g). The biphasic reaction mixture was stirred rapidly (ensuring layer mixing) at rt for 24 h. The reaction mixture was concentrated *in vacuo* until only the aqueous layer remained. The aqueous layer was decanted into rapidly stirring water (200 mL/g), and the lignin precipitate remaining in the flask was dissolved in acetone (10 mL/g) and also added dropwise into the rapidly stirring water. To the stirring mixture was added conc. HCl (approximately 20 drops/g), until the lignin was observable as a precipitate. The lignin precipitate was filtered off and dried in a vacuum oven for 16 h at 50 °C to give a brown powder.

#### Lignin General Procedure D: γ-Coupling of Butanosolv Lignin<sup>γ-oxCA</sup>

To a solution of butanosolv lignin<sup>γ-oxCA</sup> (0.4 g), HOBT (0.14 g) and EDC (0.14 mL) in DCM (15 mL) was added the amine coupling partner (2 mmol) and stirred at rt for 1 h. To the reaction mixture was added Et<sub>3</sub>N (0.32 mL) and stirred at rt for 16 h. The reaction mixture was concentrated *in vacuo*, then dissolved in the minimum amount of acetone (approximately 20 mL/g of starting lignin) and added dropwise into rapidly stirring water (200 mL/g). The precipitated lignin was filtered off and washed extensively with additional water, then dried in a vacuum oven for 16 h at 50 °C to give a brown powder.

## Acknowledgements

We would like to thank the CRICAT Centre for Doctoral Training for financial support [Ph.D. studentship to IP; Grant code: EP/L016419/1] and BBSRC Global Challenges Research Fund Impact Acceleration Account at St Andrews BB/GCRFIAA/20. CSL thanks the Leverhulme Trust for funding an Early Career Fellowship. We acknowledge the EPSRC UK National Mass Spectrometry Facility at Swansea University for mass spectrometry analysis, Sharpham Park farms for their kind

donation of walnut shells and Dr Daniel Miles-Barrett for helpful discussions.

**Keywords:** Sustainable Chemistry • Biomass • Oxidation • Green Chemistry • Lignin

- [1] P. J. Deuss, K. Barta, *Coord. Chem. Rev.* **2015**, 510–532.
- [2] A. Berlin, M. Balakshin, *Industrial Lignins*, Elsevier, **2014**.
- [3] H. Vappula, *Pulp Market Review - Energy and Pulp Business Group.*, **2011**.
- [4] J. Zakzeski, P. C. a Bruijninx, A. L. Jongerius, B. M. Weckhuysen, *Chem. Rev.* **2010**, 110, 3552–99.
- [5] I. Panovic, J. R. D. Montgomery, C. S. Lancefield, D. Puri, T. Lebl, N. J. Westwood, *ACS Sustain. Chem. Eng.* **2017**, 5, 10640–10648.
- [6] N. J. Westwood, I. Panovic, C. S. Lancefield, Springer Singapore, **2016**, pp. 183–216.
- [7] C. S. Lancefield, O. S. Ojo, F. Tran, N. J. Westwood, *Angew. Chemie Int. Ed.* **2015**, 54, 258–262.
- [8] P. J. Deuss, M. Scott, F. Tran, N. J. Westwood, J. G. de Vries, K. Barta, *J. Am. Chem. Soc.* **2015**, 137, 150522131446003.
- [9] A. Rahimi, A. Ulbrich, J. J. Coon, S. S. Stahl, *Nature* **2014**, 515, 249–252.
- [10] D. M. Miles-Barrett, A. R. Neal, C. Hand, J. R. D. Montgomery, I. Panovic, O. S. Ojo, C. S. Lancefield, D. B. Cordes, A. M. Z. Slawin, T. Lebl, et al., *Org. Biomol. Chem.* **2016**, 14, 10023–10030.
- [11] C. S. Lancefield, G. M. M. Rashid, F. Bouxin, A. Wasak, W.-C. Tu, J. P. Hallett, S. Zein, J. Rodriguez, S. D. Jackson, N. J. Westwood, et al., *ACS Sustain. Chem. Eng.* **2016**, 4, 6921–6930.
- [12] S. Constant, H. L. J. Wienk, A. E. Frissen, P. de Peinder, R. Boelens, D. S. van Es, R. J. H. Grisel, B. M. Weckhuysen, W. J. J. Huijgen, R. J. A. Gosselink, et al., *Green Chem.* **2016**, 18, 2651–2665.
- [13] S. Bauer, H. Sorek, V. D. Mitchell, A. B. Ibáñez, D. E. Wemmer, *J. Agric. Food Chem.* **2012**, 60, 8203–8212.
- [14] G. Hu, C. Cateto, Y. Pu, R. Samuel, A. J. Ragauskas, *Energy and Fuels* **2012**, 26, 740–745.
- [15] C. S. Lancefield, I. Panovic, P. J. Deuss, K. Barta, N. J. Westwood, *Green Chem.* **2016**, 19, 1203–1210.
- [16] a. a. Pereira, G. F. Martins, P. a. Antunes, R. Conrrado, D. Pasquini, a. E. Job, a. A. S. Curvelo, M. Ferreira, a. Riul, C. J. L. Constantino, *Langmuir* **2007**, 23, 6652–6659.
- [17] H. Teramura, K. Sasaki, T. Oshima, F. Matsuda, M. Okamoto, T. Shirai, H. Kawaguchi, C. Ogino, K. Hirano, T. Sazuka, et al., *Biotechnol. Biofuels* **2016**, 9, 1–11.
- [18] L. F. Del Rio, R. P. Chandra, J. N. Saddler, *Appl. Biochem. Biotechnol.* **2009**, 161, 1–21.
- [19] K. Wang, H. Yang, S. Guo, X. Yao, R.-C. Sun, *J. Appl. Polym. Sci.* **2014**, 131, n/a–n/a.
- [20] K. Wang, H. Yang, S. Guo, Y. Tang, J. Jiang, F. Xu, R.-C. Sun, *Process Biochem.* **2012**, 47, 1503–1509.
- [21] T. Renders, S. Van den Bosch, S.-F. Koelewijn, W. Schutyser, B. F. Sels, *Energy Environ. Sci.* **2017**, 10, 1551–1557.
- [22] L. Shuai, M. T. Amiri, Y. M. Questell-Santiago, F. Héroguel, L. Yanding, H. Kim, R. Meilan, C. Chapple, J. Ralph, J. S. Luterbacher,

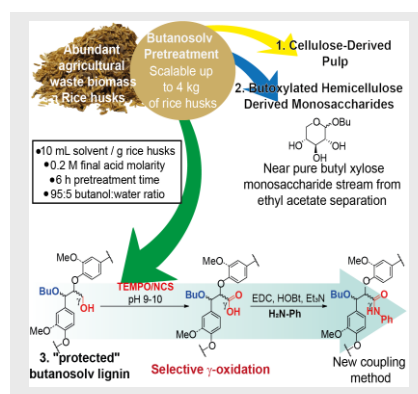
- et al., *Science* (80-. ). **2016**, *354*, 329–334.
- [23] W. Lan, M. Talebi Amiri, C. M. Hunston, J. Luterbacher, *Angew. Chemie Int. Ed.* **2017**, *5*, 1356–1360.
- [24] F. Stat, "FAO Stat," **2013**.
- [25] S. Chandrasekhar, K. G. Satyanarayana, P. N. Pramada, P. Raghavan, T. N. Gupta, *J. Mater. Sci.* **2003**, *38*, 3159–3168.
- [26] A. Salanti, L. Zoia, M. Orlandi, F. Zanini, G. Elegir, *J. Agric. Food Chem.* **2010**, *58*, 10049–10055.
- [27] R. Pode, *Renew. Sustain. Energy Rev.* **2016**, *53*, 1468–1485.
- [28] R. Saad, J. Hawari, *J. Porous Mater.* **2012**, *20*, 227–233.
- [29] F. Adam, T. S. Chew, J. Andas, *J. Sol-Gel Sci. Technol.* **2011**, *59*, 580–583.
- [30] Z. Wang, J. Yu, X. Zhang, N. Li, B. Liu, Y. Li, Y. Wang, W. Wang, Y. Li, L. Zhang, et al., *ACS Appl. Mater. Interfaces* **2016**, *8*, 1434–1439.
- [31] J. Umeda, K. Kondoh, *Ind. Crops Prod.* **2010**, *32*, 539–544.
- [32] H. Chen, W. Wang, J. C. Martin, A. J. Oliphant, P. A. Doerr, J. F. Xu, K. M. DeBom, C. Chen, L. Sun, *ACS Sustain. Chem. Eng.* **2013**, *1*, 254–259.
- [33] W. Wang, J. C. Martin, X. Fan, A. Han, Z. Luo, L. Sun, *ACS Appl. Mater. Interfaces* **2012**, *4*, 977–981.
- [34] H. Zhang, Y. Luo, L. Wu, Y. Huang, P. Christie, *Environ. Sci. Pollut. Res.* **2015**, *22*, 5908–5918.
- [35] B. C. Saha, L. B. Iten, M. a Cotta, Y. V Wu, *Biotechnol Prog* **2005**, *21*, 816–822.
- [36] N. Johar, I. Ahmad, A. Dufresne, *Ind. Crops Prod.* **2012**, *37*, 93–99.
- [37] D. Nabarlaz, A. Ebringerová, D. Montané, *Carbohydr. Polym.* **2007**, *69*, 20–28.
- [38] S. K. Singh, P. L. Dhepe, *Bioresour. Technol.* **2016**, *221*, 310–317.
- [39] M. Wu, J. Pang, F. Lu, X. Zhang, L. Che, F. Xu, R. Sun, *Ind. Crops Prod.* **2013**, *50*, 887–895.
- [40] S. Dabral, Ø. G. Hern, P. C. J. Kamer, C. Bolm, *ChemSusChem* **2017**, *7*, 2707–2713.
- [41] C. S. Lancefield, L. W. Teunissen, B. M. Weckhuysen, P. C., Bruijninx, *Green Chem.* **2018**, *19*, DOI 10.1039/c7gc00195a.
- [42] Y. Sannami, H. Kamitakahara, T. Takano, *Holzforschung* **2017**, *71*, 109–117.
- [43] S. S. Stahl, *US20170342574A1*, **2017**.
- [44] S. S. Stahl, *US20170342219A1*, **2017**.
- [45] J. Einhorn, C. Einhorn, F. Ratajczak, J.-L. Pierre, *J. Org. Chem.* **1996**, *61*, 7452–7454.
- [46] C. Jin, X. Zhang, J. Xin, G. Liu, G. Wu, Z. Kong, J. Zhang, *ACS Sustain. Chem. Eng.* **2017**, *5*, 4086–4093.
- [47] H. Liu, H. Chung, *Macromolecules* **2016**, *49*, 7246–7256.
- [48] K. Xiong, C. Jin, G. Wu, G. Liu, Z. Kong, *Chem. Ind. For. Prod.* **2016**, *36*, 115–120.
- [49] Y. Han, L. Yuan, G. Li, L. Huang, T. Qin, F. Chu, *Polymer (Guildf)*. **2016**, *83*, 92–100.
- [50] C. Wang, R. A. Venditti, *ACS Sustain. Chem. Eng.* **2015**, *3*, 1839–1845.
- [51] Pietro Buono, L. Averous, A. Duval, Y. Habibi, *ChemSusChem* **2018**, *11*, 2472–2491.
- [52] K. Isozaki, T. Shimoaka, S. Oshiro, A. Yamaguchi, F. Pincella, R. Ueno, T. Hasegawa, T. Watanabe, H. Takaya, M. Nakamura, *ACS Omega* **2018**, *3*, 7483–7493.
- [53] M. Tsakos, E. S. Scha, L. L. Clement, N. L. Villadsen, T. B. Poulsen, *Nat. Prod. Rep.* **2015**, *32*, 605–632.
- [54] A. Granata, D. S. Argyropoulos, *J. Agric. Food Chem.* **1995**, *43*, 1538–1544.



## Entry for the Table of Contents

## FULL PAPER

Rice husks were extracted efficiently using butanol as a pretreatment solvent on a variety of scales (4 g to 4 kg) giving a cellulose-derived pulp, butanol-modified hemicellulose monosaccharides and a butanol-modified lignin. This butanosolv lignin was selectively oxidised at the  $\gamma$ -position to give a carboxylic acid and tested in a coupling reaction with aniline, demonstrating a new approach for the preparation of lignin grafted materials.



*I. Panovic, D. Phillips, M. J. Gronnow, N. J. Westwood\**

**Page No. 1 – Page No. 8**

**Selective Primary Oxidation of Lignin Streams from Butanol-Pretreated Agricultural Waste Biomass**