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Evaluation of Fluid Diodes as Pulmonary Heart Valve Replacements

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EVALUATION OF FLUID DIODES FOR USE A PULMONARY HEART
VALVE REPLACEMENTS

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ABSTRACT

Children born with congenital heart disease often times suffer from severe chronic pulmonary insufficiency. Palliative treatments for this condition may come early on in the life of the patient; however, if it becomes severe enough, a pulmonary valve replacement may be required. There currently is not a permanent option for a replacements valve. Therefore, a need exists to develop a permanent solution. Knowing that the right heart circulation is more tolerant of moderate levels of regurgitation (0 – 35%) and pressure gradient (0 – 30 mmHg), this study investigates the hypothesis that a fluid diode, a motionless valve that offers low resistance to forward flow and high resistance to reverse flow, could serve as a permanent solution.

The diode valve concept was tested in vitro in a mock pulmonary circulatory system (MPCS). Transvalvular pressure gradient (TVG) and regurgitant fraction (RF%) were used to assess valve performance. The valve was tested *in vitro* over a range of pulmonary vascular resistances (PVR). *In vivo* testing was completed using a swine model. A parametric study was also done to find the effect of changing geometries on the flow regulating capabilities of the valves. Finally, flow field studies were performed using particle image velocimetry (PIV). The flow patterns, viscous shear and Reynolds shear stresses were analyzed, and the potential for platelet activation and thrombus formation was determined.

In the *in vitro* studies, the fluid diode maintained the RF% between 2% and 17% and TVG less than 17 mmHg for PVR values between 1 and 5 mmHg/Lpm. The diode performed acceptably in the animal model as well for PVR between 2.3 and 3mmHg/Lpm and pulmonary vascular compliance (PVC) between 2 to 3 mL/mmHg. The parametric study identified the angle of impingement and beta ratio as two dimensions that affect the valve performance. The total shear stress level and exposure times were found using the PIV data. The level of activation was found to be a function of PVR and, for PVR values below 6 mmHg/Lpm, the threshold reported to trigger platelet activation was not exceeded.

As a whole, the study has shown that the diode valve concept shows promise as a replacement pulmonary valve. The fluid diode is capable of regulating flow to acceptable levels for some ranges of PVR and PVC.

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NOMENCLATURE

<u>Variables and Parameters</u>

MPCS   mock pulmonary circulatory system

TVG   transvalvular pressure gradient, *also* PPG

RF%   regurgitant Fraction

PVR   pulmonary vascular resistance

PIV   particle image velocimetry

PVC   pulmonary vascular compliance

CHD   congenital heart diseases

PDA   patent ductus areteriosis

TOF   Tetralogy of Fallot

SJM   St. Jude Medical

MHV   mechanical heart valve

RBC   red blood cell

PF-3   platelet factor 3

t   residence time

GP   glycoprotein

eNOS   endothelial nitric oxide synthase

PAS   platelet activity state

LDV   laser Doppler velocimetry

X   ratio of reverse to forward flow, $X=1/(1+\lambda)$

Nomenclature (continued)

d	minor orifice diameter
D	major orifice diameter
L	overall length of the diode
b	minor width of backflow channel
B	major width of backflow channel
c	Inner ring width
ABS	acrylonitrile-butadiene-styrene
HR	heart rate
SR%	systolic ratio
RVP	right ventricle pressure
PAP	pulmonary artery pressure
DAQ	data acquisition
Q	flow rate
$Q_{forward}$	positive flow rate through valve
$Q_{reverse}$	negative flow rate through valve
mPa	mean pulmonary artery pressure
PVZ	pulmonic impedance
EOA	effective orifice area
PPG	pressure gradient, $PPG[mmHg] = RVP_{Peak} - PAP_{Peak}$
$Z(\omega)$	harmonic

Nomenclature (continued)

Z_0 zeroth harmonic

Z_1 first harmonic

CO cardiac output

x   x coordinate direction

y   y coordinate direction

u velocity in the x direction

v velocity in the y direction

m Mean velocity in the x direction

$\bar{v}$ mean velocity in the y direction

n   number of cycles

u'   velocity fluctuation in x direction

v'   velocity fluctuation in y direction

FFT   Fast Fourier Transform

DFT   Discrete Fourier Transform

SJMBV   St. Jude mechanical bileaflet valve

OTD   Omnicarbon tilting disk valve

MCS   mock circulatory system

PA   pulmonary artery

Nomenclature (continued)

I	inertance
l	length of the tubing
A	cross sectional area of the tubing
LPM	lumped parameter model
L_{VH}	upstream inertance in LPM
R_{big}	resistance of big hose to ventricle
L_{big}	inertance of big hose to ventricle
R_{VH}	upstream resistance in LPM
Q_{VH}	flow rate out of the ventricle chamber and through the hose to the test section
V_H	Volume of fluid outside the bag
C_{bag}	Compliance of the bag
Psv	Systemic venous pressure
Q_{TC}	Flow through the tricuspid check valve
P_{VC}	Pressure on the fluid
C_{RV}	Compliance
Cb	Buffer compliance
V_{BV}	Volume of fluid that sweeps the ball in the check valve along
MPA	main pulmonary artery

Nomenclature (continued)

RPA — right pulmonary artery

LPA — left pulmonary artery

RSS — Reynolds shear stress

SG — specific gravity

CFD — computational fluid dynamics

unc — uncertainty

<u>Greek letters</u>

α — impingement angle of backflow channel jet

Δp — Pressure gradient

Δt — change in time, time delay

λ — channel width ratio

β — Beta ratio; the ratio of minor to major orifice diameter, d/D

$\dot{\gamma}$ — strain rate

ρ — density

τ'_{xy} — Reynolds shear stress

τ'_{xx} — Reynolds normal stress

τ'_{yy} — Reynolds normal stress

τ_{xy} — viscous shear stress

μ — dynamic viscosity

Nomenclature (continued)

<div align="center">

<u>Subscripts</u>

</div>

min	minimum value
max	maximum value
peak	peak value
avg	average
total	total
rms	root mean square

CHAPTER ONE

INTRODUCTION

Every year, approximately 5 million people are diagnosed with valvular heart disease [1]. Valvular heart disease occurs when a heart valve does not operate properly. The two primary ways a valve may malfunction are stenosis and insufficiency. Valve stenosis is the narrowing of the valve opening. Any of the four heart valves can be affected; thereby, the condition is coined as aortic, pulmonic, mitral or tricuspid stenosis depending on which valve is affected. Valvular insufficiency is the failure of the leaflets to completely close; thus, allowing for the flow of blood across the valve when it is closed. This is called aortic, pulmonary, mitral or tricuspid regurgitation, depending on location.

Heart valve diseases are both congenital and acquired conditions. Some examples of conditions that develop before birth include absent valves, valves of the wrong size or valves that are malformed or attached incorrectly [1]. Rheumatic fever is an example of a condition that can cause heart valve defects. Heart attacks, hypertension and cardiomyopathy are also potential causes of heart valve disease. Valvular stenosis and insufficiency can both reduce the efficiency of the heart and many cases require surgical treatment. Approximately 250,000 valve repairs or replacements take place a year [2, 3].

While the most commonly affected valves are the aortic, mitral and tricuspid, there are conditions that affect the pulmonary valve as well. As stated previously,

pulmonary stenosis can occur in addition to other pulmonary valve defects such as pulmonary atresia and Tetralogy of Fallot [4]. If the valve is severely stenosed or regurgitant, it must be replaced. Standard replacements are allografts, xenografts, bioprosthetic valves or mechanical prostheses. Bioprosthetic valves are not robust enough to last long enough in patients that receive it at a young age as they can degrade over time. Calcification of the valve leaflets can occur at higher rates in younger patients [5]. Whereas mechanical valves require the patient to take anti-coagulants and may also be subject to mechanical failures [4]. Another type of bioprosthetic valve used to treat pulmonary insufficient is a bovine jugular vein with a valve. It can be implanted percutaneously. However, it has limited applicability due to size restrictions and structural issues with the stent [6].

Babies born with pulmonary valve defects may require many operations during their lifetime. Early on in life, the patients have palliative repairs performed. Some patients can lead a normal life after this repair. However, the repair may leave the pulmonary valve insufficient. This will cause the patients to live a life of limited activity and will lead to an increase in the workload on the heart. The treatment for an insufficient valve is a pulmonary valve replacement. For those born with a congenital defect, this surgery may occur when the patient is in late adolescence or early twenties.

The pulmonary heart circulation differs from the systemic circulation due the lower operating pressures. The right heart is more tolerant to increased pressure gradient and regurgitation.

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The purpose of this study is to determine if an artificial replacement without movable and wearable parts can act as a suitable alternative to existing prostheses for application in the pulmonary position. Will a valve with flow channels that work against reverse flow, known as a fluid diode, provide adequate performance in the pulmonary position? The criteria used to evaluate the performance include the level of regurgitant flow, the pressure gradient across the valve and the mechanical performance of the valve. A mock circulatory system tests the proposed designs *in vitro*. The flow field generated by the valve is also observed for any flow anomalies and to determine the levels of shear stress created by the valve.

CHAPTER TWO

BACKGROUND

Pulmonary Circulation in a Healthy Heart

The heart is made up of four chambers and acts as two pumps in series to circulate blood throughout the body (Figure 2.1). The upper chambers of the hearts are the atria. The lower chambers are the ventricles. There are four valves in the heart that behave as check valves. They exist to keep the blood flowing in one direction as it is pumped through the heart. The mitral (bicuspid) and tricuspid valves are located in between the chambers. The aortic valve is between the left ventricle and the aorta. The pulmonary valve is between the right ventricle and the pulmonary artery.
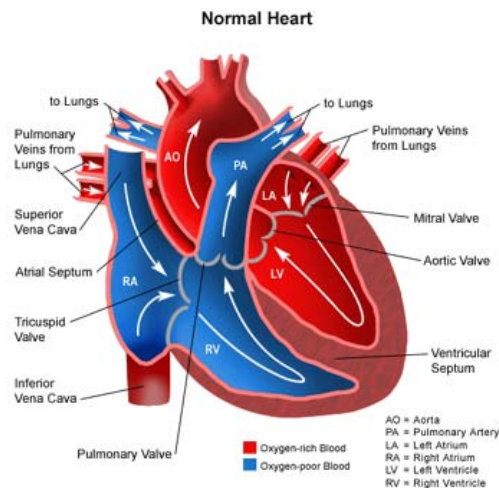
Figure 2.1. Schematic of human heart

The left ventricle supplies blood to the tissue and organs in the body as a means of delivering nutrients and oxygen. During a relaxation phase of the heart, oxygenated blood returns to the left atrium by way of the pulmonary vein. The ventricular pressure during diastole is around 0 mmHg. Therefore, the pressure in the atrium is slightly higher. This atrio-ventricular pressure drop in addition to a slight atrium contraction causes the mitral valve to open and blood to flow from the atrium to the ventricle. Systole occurs when the ventricle contracts and consequently the intraventricular pressure increases. Simultaneously, the mitral valve closes and the aortic valve opens and systemic circulation takes place. Blood flows through the aorta to the body. The oxygen depleted blood returns to the right atrium at low pressure through the superior and inferior vena cave. Just as on the left side, an atrio-ventricular pressure drop and a slight contraction in the atrium causes the tricuspid valve to open and the right ventricle to slowly fill with blood from the right atrium. When the right ventricle contracts and the tricuspid valve closes, the pulmonary valve opens and blood flows into the pulmonary artery. The artery branches off into the left and right lungs. The blood is re-oxygenated and returned to the pulmonary vein. The cycle returns to its original state.

In a normal adult the average heart beat is 70 beats per minute or about 85 ms per cycle. Moreover, this changes based on the level of activity (exercise or sleep) [7]. In children, the heart beat is faster. There are periods of contraction (systole) and relaxation (diastole) during the cardiac cycle. Systole lasts about one third of the cardiac cycle, typically 200-300 ms [2]. The amount of blood that is pumped during one beat of the

heart is the stroke volume. The volume pumped every minute is the cardiac output or the flow rate. Cardiac output is the product of the heart rate and the volume ejected by the heart per stroke (stroke volume) [7]. The cardiac output through the circulatory system is approximately 5 Lpm at rest and 25 Lpm during heavy exercise [8]. At 5 Lpm, the resulting peak velocities are 0.75 ± 0.15 m/s in healthy adults and 0.9 ± 0.2 m/s in children through the pulmonary valve [2].

While the flow rates are equal on both sides of a healthy heart, the pressures on the right side of the heart are lower than that on the left side. The pulmonary and tricuspid valves experience pressures up to 30 mmHg [2]. This is in contrast to the aortic valve which holds 100 mmHg when closed and the mitral valve that withstands 150 mmHg [2]. This difference is a result of the systemic resistance being much higher than the pulmonary resistance simply because there are more vessels through which the blood flows. The lower pressures result in abnormal valve behavior. The pulmonary vessels resistance is approximately one tenth of the resistance in the peripheral vessel network [7].   The resistance is best characterized by the pulmonary vascular resistance or PVR. PVR is the ratio of mean pulmonary artery pressure and the mean cardiac output. It is the resistance of the right ventricle to pulmonary circulation [9].   Normal PVR ranges between 1 and 5 mmHg/Lpm with an average of 2.0 mmHg/Lpm [10]. Slife, et al. [11] reported values of 20.0 dynes-s/cm^5 which is equal 0.8 ± 0.1375 mmHg/Lpm during periods of rest. Along with resistance, arterial compliance exists. Pulmonary compliance is the change in volume that occurs within the blood vessels and heart with changes in

pressure. It is the ratio of the stroke volume of the heart to the mean pulmonary artery pressure. Reported values for compliance range from 4 to 8 ml/mm Hg [11, 12]

Diseases affecting the pulmonary valve make up around 25% of all congenital heart valve diseases [13]. Moreover, because of the hemodynamic differences between the left and right sides of the heart, the pathology and treatment concerning pulmonary valves may differ than that of the aortic valve. Therefore, the characteristics of the pulmonary valve diseases and treatments are specifically studied in this case.

Diseases of the Pulmonary Heart Valve

There are many congenital heart diseases (CHD) that can affect the pulmonary valve conduit. One such condition is pulmonary atresia which is the absence of a pulmonary valve altogether. As a result, blood cannot flow from the right ventricle to the pulmonary artery. Blood only reaches the lungs by way of a patent ductus arteriosis (PDA). Pulmonary atresia can be treated medically to keep the PDA open or surgically by implanting a shunt or a complete repair.

Another disease is pulmonary stenosis. This is when a valve leaflet is malformed. Pulmonary stenosis can lead to restricted flow across the valve due to a sticking leaflet. This restriction causes higher than usual pressure gradient across the valve and this in turn makes the heart work harder to maintain cardiac output. Pulmonary stenosis comprises roughly 10% of all CHDs [14]. Mild stenosis is tolerable and usually does not require intervention. Severe stenosis produces gradients of 40 mmHg or greater [15].

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Stenosed valves can also become leaky or insufficient. Insufficient valves are those in which blood flows back (regurgitates) from the pulmonary artery into the ventricle. Severe insufficiency can lead to an increase in the workload on the heart. The right ventricle can also begin to dilate as a result. Stenosis can be treated with balloon valvuloplasty. However, in severe cases an operation may be required to repair or replace the valve [16]. Since higher than usual pressure gradients can over work the heart, a design constraint for the proposed valve is to produce a pressure gradient of less than 25 mmHg.

Another condition affecting the pulmonary valve is pulmonic valve endocarditis. This is an infection of the valve. It rarely occurs in people with healthy hearts; however, patients with preexisting conditions are susceptible [17]. Surgical intervention is sometimes necessary for when treating pulmonic endocarditis. This may involve either a valve repair or replacement [17].

Pulmonary stenosis and atresia together also play a role in another condition: Tetralogy of Fallot (TOF). This condition affects anywhere between 9-14% of all babies born with cardiovascular defects [13]. There are four features to TOF: a ventricular septal defect, the obstruction of the right ventricle to the lungs (either by varying degrees of pulmonary stenosis or pulmonary atresia), the aorta lies directly over the ventricular septal defect, and the right ventricle develops thickened muscle [16]. Babies born with TOF are often blue; hence, referred to as blue babies, because oxygen poor blood is being pumped throughout the body. Newborns undergo a temporary operation in which a shunt

is built between the aorta and the pulmonary artery in order to provide enough blood flow to the lungs. A complete repair is done when the child is approximately 6 months old. This involves closing the ventricular defect, removing the thickened muscle, repairing or removing the pulmonary valve and enlarging the peripheral pulmonary arteries that go to both lungs [16].

The correction of Tetralogy of Fallot often leads to pulmonary insufficiency or regurgitation which results in right ventricle dilation [18-21]. Tulevski et al. [22] define mild pulmonary regurgitation as 10-30 mL per beat. At a nominal heart rate of 70 beats per minute and cardiac output of 5 Lpm, mild pulmonary regurgitation is 0.7 – 2.1 Lpm for a regurgitation fraction of 14 - 42%. This amount of regurgitation is representative of a patient who is asymptomatic or minimally symptomatic. If regurgitation is severe enough to cause right ventricle dilation, a pulmonary valve replacement becomes necessary. For the short term to medium term, Conte [23] states that clinical studies fail to demonstrate adverse effects of pulmonary regurgitation as long as there are no other cardiac problems. In the long term, however, pulmonary regurgitation can result in right ventricle dilation and failure. Thus, it is the goal of this study to have a valve design on the low end of mild regurgitation with a regurgitant fraction of 20% or less.

<u>Types of Replacement Valves</u>

There are many types of prosthetic and replacement valves that can be used as a heart valve. The next section will briefly review each type of valve and any associated

complications, as understanding of the side effects are critical in establishing design criteria for a new prosthetic valve.

<div align="center">Mechanical Replacement Valves</div>

The four most commonly used prostheses are caged ball, tilting disc, bileaflet, and bioprostheses [2]. There have been several studies evaluating and comparing the different types of valves [2, 3, 24-26]. Butany, et al. reviewed of all contemporary heart valves so that information is readily available [3]. This helps in the identification of the different valves as well as the known complications that may be associated with each type. All mechanical valves have three components: an occluder or leaflet, housing, and sewing ring [3]. The three most common types of mechanical valves described are the ball-in-cage, single leaflet, and bileaflet. Figure 2.2 shows images of these three types of valves.

Figure 2.2 Examples of mechanical valves: (a) ball in cage, (b) tilting disk, and (c) bileaflet

Ball-in-cage valves have a ball as the occluder and a cage like structure as the housing. This valve produces lateral flow around the ball [3]. The Starr-Edwards ball-in-cage prosthesis was the first commercially available mechanical valve. This design debuted in the 1960s. It was exclusively used in the aortic and mitral positions. Early complications included the silicone rubber balls absorbing lipids, disposing them to early deterioration and variance. This led to one of several modifications that have been made to the original design [25]. Butany, et al. [3] reported other problems such as damage to the ball, thrombus formation, pannus formation, and the occurrence of hemodynamic injury. These problems could keep the ball from seating correctly or allow it to get stuck in an open or closed position. *In vitro* studies on the Starr-Edwards valve have also shown its poor hemodynamic performance [2]. Despite its problems, it was one of the most prescribed prosthesis and it is still used on occasion [3]. Over 250,000 had been implanted at the time of Gott, et al.'s publication [25]. Other researchers developed ball valves for use as a heart valve replacement. Among the areas that on which these designs focused was decreasing ball variance or reducing thrombus formation; however, many of these have ceased production [25].

Another type of mechanical valve is the tilting disc, or single leaflet valve. Tilting disc valves have a single leaflet on a hinge as the occluder. Most contemporary valves are made of pyrolytic carbon with a graphite coating. There are some metal components and a sewing cuff made of synthetic fabrics [3, 25]. The leaflet opens and closes due to the pressure gradient created by the heart. Tilting disc valves produce a central flow

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pattern [3]. There are many types of tilting disc prostheses including the Björk-Shiley and the Medtronic-Hall tilting disc [2, 3, 25]. The Björk-Shiley was first introduced in 1969 and has since been discontinued [25]. Butany, et al. [3] reported one such problem with this design was thrombus formation at the site of the hinging mechanism that can cause them to have restricted or stopped leaflet motion and pannus on the sewing ring leading to valve dysfunction. The Björk-Shiley ceased production in 1986; however the Medtronic–Hall continues to be the most commonly used tilting disc [2]. The studies show that tilting disc valves exhibit a low rate of valve-related complications and excellent hemodynamic characteristics especially when anti-coagulant therapy is used [2, 3, 25]. Though this valve type is primarily used as aortic valve or mitral valve replacement, it has also been used in the pulmonary valve position.

The final category of commercially available mechanical valve is the bileaflet valve. Bileaflet valves have two occluder discs that pivot on separate hinges. Like the single disc valve, these also open and close due to the imposed pressures created by the heart and they are composed of similar materials. It is primarily used as an aortic or mitral valve replacement, yet use as a pulmonary valve replacement is not unusual. The first bileaflet valve was the Gott-Dagget design; however, the St. Jude Medical (SJM) is the most commonly used. The SJM was first introduced in 1977 and more than 1.3 million valves have been implanted [25]. While the valve has since undergone many design iterations, the basic design has remained virtually unchanged [3, 25]. The advantage of the bileaflet valve is that it provides symmetric and relatively undisturbed

flow, which is important to keep platelet activation and thrombus formation low [27]. There are many cases of the St. Jude Medical valve having been used in the pulmonary position [28-34]. Some complications with these valves include a small number of mechanical failures, the potential for thrombus obstruction and pannus formation. Despite these issues, the bileaflet valve is regarded as the best alternative in mechanical valve design. This type of valve is of particular importance to this work because it serves as a comparative benchmark for the new styles of valves that were tested.

Side Effects of Mechanical Valves

Anticoagulant therapy is generally required in patients that receive a mechanical replacement because of the complications associated with using mechanical heart valves [4, 29]. Mechanical heart valves (MHV) have a reputation of causing thrombus formation even more so when placed in the pulmonary position. Thrombus formations can hinder the motion of the valve mechanism and cause it to be stenosed, regurgitant, or stuck in the open or closed position. Miyamura, et al. [29] showed complications as a result of using a St. Jude bileaflet valve in the pulmonary position. Similarly, another study found that several of their patients experienced life threatening complications due to thrombus formations [31]. Neither study recommended SJM valves for use in the pulmonary position in children. Meuris et al. [35] compared monoleaflet behavior to that of bileaflet valves in an animal study. They found that the bileaflet valves were subject to more severe thrombosis than the monoleaflet valves when placed in the pulmonary position. There are other reports with similar findings regarding thrombosis

in replacement valves [30, 36, 37]. There is one reported case in which anticoagulant therapy was not maintained, yet the implanted valve showed no signs of thrombus [33]. Thrombus formation can not only lead to valve malfunctions, it can also create a thromboembolism. This is a piece of thrombus that travels downstream and clogs a blood vessel. There are many ways in which thrombus formation can be detrimental to mechanical valve performance. It is a phenomena closely related to the fluid dynamic performance of the valve.

Another complication that can hinder the performance of a mechanical valve is pannus growth. Pannus is tissue overgrowth on a portion of the valve and it can also clog or stenose a valve. Deveri et al. [38] found that pannus growth was just as likely as thrombus formation for bileaflet and tilting disc valves in the mitral and aortic positions. A study by Ilbawi et al. [28] found that pannus formation in bileaflet valves is worse in when it is used in the pulmonary position versus the aortic and mitral positions. They studied mechanical valves in the pulmonary position in children and found that pannus formation was a primary cause of valve malfunction. Fibrous tissue growth caused leaflet immobilization. Pannus formation is a problem in the pulmonary position due to the low operating pressures. Therefore, this factor must be taken into consideration in the design of new valves.

Patients receiving MHVs are required to be on anticoagulent therapy in order to reduce thrombus formation due to elevated shear stress levels across the valve. However, anticoagulation therapy leaves the patient at risk to bleeding complications [36, 39].

Since the blood cannot clot as quickly, it takes longer for a wound to heal. If the wound causes internal bleeding, the situation is even more dangerous and can lead to death. Patients on anticoagulant therapy are susceptible to complications in the event of a need for emergency surgery.

Mechanical malfunction and failure is another potential risk of using a mechanical valve. A mechanical valve is subject to many opening and closing cycles; therefore, some mechanical mechanisms will fail to operate properly or at all. In a study by this research group, both bileaflet and a monoleaflet valve were shown to exhibit aberrant behavior, such as leaflet bounce or incomplete closure when tested in vitro in the pulmonary position [40]. The bileaflet valve was shown experience leaflet flutter at PVR = 2.0 mm Hg/Lpm. The monoleaflet valve saw an onset of aberrant behavior at PVR = 1.6 mmHg/Lpm.

In addition to mechanical misbehavior, the valves can mechanically fail. As previously stated, Butany et al. [3] reported that one type of failure of the early ball-in-cage valves was that the balls tended to crack. Malouf et al. [41] reported a split disc failure in the Star-Edwards disc prosthesis after 27 years of operation in the patient. The St. Jude Medical bileaflet valve has shown much lower mechanical failure rates. In a study by Chang et al. [36], over 600 SJM valves were implanted with no reports of structural deterioration during long-term follow-up. Emery et al. [39] reported similar success with the SJM valve performance; they reported zero mechanical valve failures in their follow-up study of St. Jude Medical recipients [39]. Hence a standard for low rates

of mechanical valve failure has been established for any newly designed replacement valve.

Biological Replacement Valves

In addition to mechanical heart valve replacements, there are also biological replacement valves. Worldwide, over 45% of the implanted replacement valves are biological [5]. There are two types of biological replacements: bioprosthetic valves and tissue heart valves. There are four types of bioprosthetic valves in use, and Butany et al. [5] give a substantial review of these different types. The four categories are the stented porcine valve, stented pericardial valve, stentless porcine valve, and homografts. The first three mentioned use porcine or bovine tissue whereas homografts are harvested from human cadavers and are accordingly more difficult and expensive to acquire. The advantage of using bioprosthetic valves is that they more closely imitate the flow and material properties of their native counterparts. The downside of this is that they are not as robust other prostheses, as they tend to calcify and tear [42]. This is especially true when they are implanted in children. Ilbawi et al. [28] state that increased calcium metabolism rates and the turbulent flow due to children's smaller valve orifice area lead to accelerated valve degeneration. Fukada et al. [43] additionally state that size mismatches and growth interfere with pulmonic placement of bioprostheses in children.

Despite the reputation for bioprosthetic valves to be short on robustness, biological replacement valves have been used to replace the pulmonary valve in most cases. However, these valves can deteriorate over time and make it necessary for the

patient to undergo one or more reoperations [4, 43]. So they may not be the best pulmonary valve replacement option in younger patients.

More recently, focus has shifted to percutaneous replacement of pulmonary valves. Bonhoeffer, et al. [6] successfully implanted a stent mounted, bovine jugular vein with a native valve by catheter in a 12 year old patient. This eliminated the need for the patient to undergo open heart surgery. Since this time other patients suffering from right ventricular outflow tract dysfunction have been treated in this manner. In a Lurz and Bonhoeffer [44] review of these cases, it was found that significant improvement has been made in the area of percutaneous pulmonary heart valve replacements. Yet, while there is improvement, there are also limitations and complications. At the time of the 2008 review, safe implantation was expected only for patients with conduit diameters of 22 mm or less [44]. Thus, there are limited anatomies that can accept the stent. Moreover, the most common complication was a fracturing stent [45].

It is evident that there are concerns over the robustness of both the mechanical and bioprosthetic valves, especially when placed in the pulmonary position. Therefore, the basis of the proposed valve design is that it will show marked improvement in robustness and remove the need for the patient to take anticoagulants.

<u>Effect of Shear Stress and Flow Anomalies</u>

The most serious problems with mechanical heart valves are related to thrombus formation. They include thrombosis, which leads to mechanical malfunction and the

development of thromboembolisms. Moreover, patients must take anticoagulants that can lead to bleeding events. Mechanical heart valves are disruptive to the normal flow in the heart and vessels. Areas of high shear stresses, turbulence and rotating flow are created around the leaflets. These regions of shear stress have been shown to induce thrombus formation [46]. One of the first steps in thrombosis is the activation of platelets. High shear can lead to damage of red blood cells or vessel walls which in turn can lead to the activation of platelets. Many studies have been conducted to determine how shear stresses may affect blood cells, platelets, and vessel walls [47-53]. These studies have shown that the damage to red blood cells (RBCs) and platelets is dependent on the magnitude and exposure time to certain levels of shear stress.

In 1972, Leverett et al. [50] found a threshold level of shear stress of 1500 dynes/cm^2 for an exposure time on the order of 10^2 seconds at which extensive blood cell damage occurs. They also summarize prior studies on the effect of shear stress exposure time on hemolysis. There was much disagreement amongst the threshold level of damage for RBCs between all of the works because of the varying levels of exposure time.

Additional studies since the summary provided by Leverett et al. [50] present results that further support that stress level and exposure time both play a role in the damage to red blood cells and as well as platelet activation. Ramstack et al. [54] subjected platelet rich plasma to varying levels of shear in Poiseuille flow in tubes. The residence times were also varied. They used the release of platelet factor 3 (PF-3) as an indicator of platelet activation. They found that the amount of stimulation as a function

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of the product of the shearing strain rate ($\dot{\gamma}$) and the residence time (t). At $\dot{\gamma}t \geq 10^3$, the availability of PF-3 begins to increase.

Sallam and Hwang [51] investigated the effect to Reynolds shear stresses on hemolysis and found a threshold of 4000 dynes/cm^2 for an exposure time of roughly two minutes (10^2 seconds), to be the point at which hemolysis occurs. This is on the same order of magnitude of the results found by Leverett et al. [50]. Hung et al. [48] found that platelet activation can take place for shear stress values of 100-300 dynes/cm^2 for a similar exposure time.

Stein and Sabbah [52] attempted to quantify the effect of turbulence on thrombus formation by implanting shunts in dogs, one that promoted laminar flow and another that created turbulent flow with an orifice plate. By measuring the weight of the thrombi in shunt flow case, they found that the turbulent shunt accumulated more thrombi than the laminar case. Moreover, the weight of the thrombi appeared to be related to the level of turbulence intensity; thus, they showed that the turbulence can contribute to the formation of thrombi. In a later paper, Stein and Sabbah [53] reviewed many studies and summarized the effects of shear stress on platelets and RBCs. They reported that platelet lysis had previously been observed to take place at shear levels of 165 dynes/cm^2 for short exposure times (on the order of milliseconds). However, at level of less than 100 dynes/cm^2 no damage had been seen at high exposure times. Extremely high shear stresses of 15,000 dynes/cm^2 and exposure times of 5 milliseconds, or 75 dynes-s/cm^2,

were linked to platelet lysis. Thus, the importance of exposure time lead to the need to understand the effect of turbulent shear stresses.

In another study, steady flow through an arterial stenosis was modeled using experimental and numerical methods [55]. They calculated the *level of activation* which was the cumulative product of shear rate and exposure time along a platelet path. The level of activation reached 500 at a Reynolds number of 3,600. This is equivalent to 17 dynes-s/cm^2 for blood plasma with a viscosity of 0.035g/cm-sec and is less than the threshold found by Ramstack et al. [54] to activate platelets.

As a result of the connection between the level of shear stress and exposure time of that stress on a platelet or red blood cells, and knowing that artificial valve devices can disrupt natural flow behavior, the design and development of prosthetic heart valves includes a more directed study of resulting hemodynamics. The literature includes studies that focused on the turbulent shear stress measurements around prosthetic heart valves [46, 56-58].

The correlation between the level of stress and the time at that stress level has been demonstrated by the previous studies. Lim et al. [59] conducted PIV studies on pulsatile flow through bioprosthestic valves in the aortic position. They found the maximum shear stresses of 3469 dynes/cm^2 at 120 ms after aortic valve opening. Also, using models established by Giersiepen et al. [60], they estimated shear stress related blood damage. Using this model to account for shear stress and exposure time, they

showed that a particle travelling through the highest region of shear stress experienced shear stresses sufficient for blood damage.

In addition to interfering with the mechanical behavior of a valve, thrombus can also break away and travel down the blood stream as an embolus. Bluestein, Rambod and Gharib [61] conducted numerical and experimental flow studies of a MHV and they found that regions of high turbulence, shear stress, and recirculation enhance platelet activation and deposition. They also revealed interacting shed vortices and concluded that this provided an opportunity for platelets to get trapped in wakes where they can aggregate. Thus, these aggregates can travel away from the valve and become free emboli. In regions of slow moving separated flow these thrombus formations can attach themselves to the valve, which can then lead to the aforementioned impedance of valvular motion. In another study, Bluestein, et al. [27] conducted numerical simulations of turbulent pulsatile flow characteristics past the SJM valve and interactions of the platelets with the flow. They showed that platelets traveling close to the surfaces of a mechanical valve were more likely to activate and thromboembolize and that implementation techniques could enhance the risk of cardioembolism. Thus, areas of flow stasis can lead to platelet aggregation.

In the case of any unnatural flow such as that created by a prosthetic valve or even and severely stenosed valves or conduits for example, can lead to high wall shear. Elevated wall shear has thusly been implicated in the platelet formation. Holme et al. [62] stated that natural shear rates are around 420 s^{-1}. They experimented with human

blood and assessed platelet activation by measuring activated glycoprotein (GP) IIb/IIIa by aminophospholipid translocation. They found that at high shear rate of 10500 s^{-1} (367 dynes/cm^2 at 3.5 cP), platelet activation was increased. However, at natural shear rates of 420 s^{-1} and levels up to 2600 s^{-1}, platelet activation did not occur. That corresponds to wall shear stresses of 14.7 and 91 dynes/cm^2, respectively. This was similarly related to exposure time. In addition to wall shear being linked to triggering thrombus formation, it has also been shown to effect the expression of endothelial nitric oxide (eNOS) synthase [63-65], a vasodilator. One study found that the arterial levels of shear stress of 25 dynes/cm^2 can elevate eNOS.

So, in addition to the need to create a more robust valve, the valve must also cause as little disturbance to the flow as possible. The level of turbulent stresses and the time that the blood is exposed to these forces should be below the threshold known to cause damage. Moreover, any areas of flow stasis should be minimized to lower the chance of platelet aggregation.

Experimental Methods

There are two basic ways that heart valves can be studied, *in vivo* and *in vitro*. *In vivo* methods involve taking flow measurements while the subject is still alive; *in vitro* methods involve the testing of the valves in a laboratory test stand. It is clear that *in vivo* measurements offer advantages, because the heart valves can be tested in their natural environment. However, *in vivo* methods are more complicated and dangerous to perform.

Thus, it is important to perform valve studies *in vitro* first in order to validate a suitable prosthetic design before proceeding to *in vivo* studies.

Mock Circulatory Systems

There have been many studies that have focused on valve evaluation outside of the body. *In vitro* evaluation offers a reproducible, reliable, and consistent platform for comparative testing and offers flexibility in the types of testing and evaluation. *In vitro* setups seek to match the physiological performance of the circulatory system without necessarily taking on the form of the components. They usually consist of a pump, systematic resistance and capacitance elements, which act as blood vessel resistance and compliance, a method to vary the system pressure, and a test section where the valve is mounted. This test section is constructed to take on the geometry of the area that is being studied such as the aorta or pulmonary artery.

Many mock circulatory loops have been constructed. Early systems modeled steady flow loops that included a pumping source, flow control valves and a source to measure flow rate and pressure [57, 66-68]. Bluestein and Einav [69] point out a problem with the steady flow approach. They found that flow turbulence through heart valves peaks during the mid diastole phase of the cardiac cycle, which cannot be characterized in steady flow experiments. To this end, most mock circulatory loops are constructed with pulsatile flow capabilities. A follow up to Lim et al.'s [59] steady flow study was conducted using a pulsatile flow system. These setups were also built to simulate systemic flow circulation.

The literature is filled with descriptions of pulsatile flow loops that model left heart circulation [46, 59, 70-76]. For example, Pantalos et al. [77] designed a mock circulatory system that mimicked the Frank-Starling response for normal, heart failure and cardiac recovery condition. This system incorporated a flexible polymer sphere as the atrium chamber. The ventricle is a flexing, polymer sac inside a pressurized chamber. The simulation of the ventricle contraction was accomplished using metered pulses of compressed air. The compliance and resistance was modeled with four chambers. There were pressure taps and flow probes throughout the system that took measurements at different points in the system.

Timms et al. [78] built a system that models the systemic and pulmonary circulation. This system was similar to that of Pantalos et al. [75], except it included the right heart circulation. The atria chambers were PVC tanks that were open to atmosphere. The heart was pneumatically actuated. The chambers were made of PVC piping with capped end and one tapped so that pressurized air could be input. The compliance chambers were Windkessel vessels, also made from PVC piping. Pipe test plugs were used to secure the amount of air in the chamber. The systemic and pulmonary vascular resistances were affected by proportional control valves.

There are fewer systems that model the pulmonary circulation [34, 79-81]. One example of a mock pulmonary circulatory system is the one used by Philpot [79, 80] to do *in vitro* testing of valves in the pulmonary position. This system used a pneumatic ventricle to create the pulsatile flow. A glass model of the pulmonary artery was used.

The flow rate division was controlled using ball valves and the pressure was varied using two compliance sections.

Medical devices, especially cardiovascular devices, must be proven to not only successfully operate but also to not create any harmful side effects. While most situations can be modeled experimentally, *in vivo* studies are still necessary in testing those things that cannot be mimicked. Animal testing is a way to validate the designs of devices prior to clinical evaluation in humans. Some animals models that have been used to conduct *in vivo* studies on heart valves are calves, goats, sheep, dogs and pigs [82-88]. The focuses of animal studies include improvements in structural integrity, anti-thrombogenicity, anti-calcification and implantation techniques. There are similarities between the coagulation cascade, platelet function and the platelet-leuckocyte-enthothelial cell interaction of humans and pigs. These make pig models more suitable for analyzing thrombosis and platelet activation resulting from prosthetic valves [88]. Sheep models are preferred for chronic evaluation and studies of surgical techniques [82].

Choo, et al. [85] discuss the ways the hemodynamic performance of prosthetic heart valves can be measured during *in vivo* tests. In this study, valvular function was monitored with color Doppler and by continuous or pulsed wave Doppler. The transvalvular pressure gradients were calculated from the maximum velocity measurements across the valve. This blood velocity data was obtained using continuous-wave Doppler as well.   Pulsed wave time velocity integral data along with the known cross sectional area of the valve were used to find stroke volume. The cardiac output was

in turn calculated by multiplying the stroke volume by the heart rate. Other studies focusing on platelet activation evaluated prosthetic valves by taking platelet activity state (PAS) assay measurements before and after implantation [82, 89].

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<div align="center">Particle Image and Laser Doppler Velocimetry Techniques</div>

The literature has shown that it is necessary to understand the potential of a prosthetic heart valve design to lead to thrombus formation or other damage to the blood or blood vessels. In regards to *in vitro* studies, optical flow measurements have been used to study the flow through prosthetic heart valves. Both laser Doppler velocimetry (LDV) and particle image velocimetry (PIV) have been used to measure cardiovascular flows [46, 56-59, 61, 68, 73, 74, 90-102]. Laser Doppler velocimetry (LDV) has a high degree of accuracy, spatial and temporal resolution and it has been used to measure the turbulent stresses in the flow through prosthetic heart valves [56-58, 90, 95, 99-103]. The range of how PIV used is from the simple, such as presenting the flow field mappings [93, 95], to calculating vorticity fields and viscous shear stresses [61, 74, 97], to determining turbulent shear and normal stresses [59, 68, 90] .

In the study by Bluestein et al. [61] in which flow and vorticity fields surrounding the leaflets of an bileaflet MHV were plotted in order to identify areas of that platelets could potentially aggregate. The PIV measurements showed three jets are formed past the valve; one is between the two leaflets and the other are between the leaflets and the

housing ring. They also observed wake regions extending from both leaflets, and that the vorticity values ranged up to 500 s^{-1}.

In studies by Lim et al [59, 68], both steady and pulsatile flow through aortic bioprosthetic valves were analyzed. In addition to mapping flow, they also calculated turbulent stresses. They compared similar flow rates and determined that the turbulent shear stresses in the pulsatile flow increased by as much as 1.2 to 1.6 times over that measured in the steady flow case. The maximum Reynolds shear stress, measured at peak systole, was 3469 dynes/cm^2. The maximum Reynolds normal and transverse axial stresses were 4963 and 2425 dynes/cm^2, respectively.

There are also studies using and comparing both methods. For instance, Browne et al. [92] collected steady flow measurements on an aortic model using both LDV and PIV methods and used both methods to plot the flow fields and find turbulent stresses. They found that, as expected, PIV could efficiently measure velocity; however, the maximum turbulent shear stresses found using PIV were higher than the LDV results. Thus, they concluded that a combination of PIV and LDV may be more suitable for turbulent flow areas. A later comparison of dynamic PIV, with use of a high speed camera, and LDV methods showed better agreement between the two types of Reynolds stress measurements [90].

<u>The Fluid Diode</u>

The purpose of a pulmonary heart valves is to prevent blood from flowing backward into the right ventricle from the pulmonary artery. In the specific situation of treating pulmonary insufficiency in patients born with congenital heart disease, the circumstances yield a certain set of requirements. The patients are younger in age, and current solutions lack the longevity needed to keep them from needing to undergo reoperations. So, robustness and longevity are important. Also, their quality of life should be kept as high as possible, so the need for anticoagulants should be avoided. The valve should disrupt the blood flow as little as possible, meaning that regions of high shear levels and of flow stasis should be minimized.

The above parameters or ideals would apply for any type of prosthetic heart valve. However, the cited differences between the operating pressure of the pulmonary and the systemic circulations afford for a different and less strict tolerance on the pressure gradient and regurgitation. As stated earlier the right heart circulation can handle mild regurgitation and pressure gradient. Taking these allowances into account and considering the other desired design specification, a novel concept for a replacement pulmonary heart valve, the fluid diode valve, was developed.

A fluid diode is an engineering device that impedes reverse flow with their geometry. The resistance to flow in the reverse direction (retrograde flow) is higher than for that of forward flow (antegrade flow). One example of a fluid diode is a nozzle. A simple nozzle is shown the in Figure 2.3 below. Forward flow (the direction of the

arrow) is encouraged by the decreasing cross sectional area. The velocity increases as fluid flows from higher pressure to lower pressure. For flow in the opposite direction, the fluid would be flowing against adverse pressure gradients and therefore, flow would be restricted.
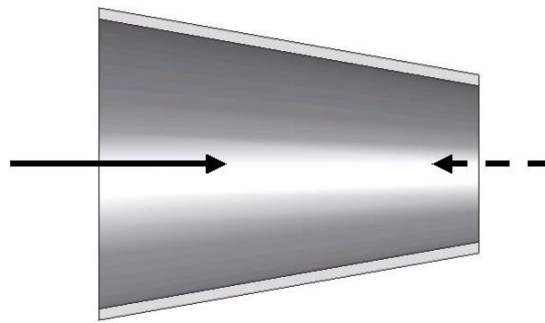
Figure 2.3 Standard Nozzle

The Tesla diode was first developed by Nicola Tesla and was described in his valvular conduit patent in 1920 [104]. Figure 2.4 is from Tesla's patent describing the motionless device. Forward flow is from right to left. The layout of the channels makes it so that the flow will proceed through the device nearly undisturbed and with minimal head loss. However, upon flow reversal, the fluid is directed into the curved passages. The fluid exits the flow passages moving in the direction of forward flow; thus, it makes

it difficult for any net backflow to occur. In his patent, Tesla says, "It will be readily observed that the resistance offered to the passage of the medium will be considerable even if it be under constant pressure, but the impediments will be of full effect only when it is supplied in pulses…" [104]. Thus he implies that the fluid diode is more effective when used with pulsing flow, as would be the case with the circulatory system. Therefore, it is hypothesized that the adaptation of this device to a prosthetic heart valve could yield a means to regulate blood flow by a device with no moving parts and with minimal backflow.
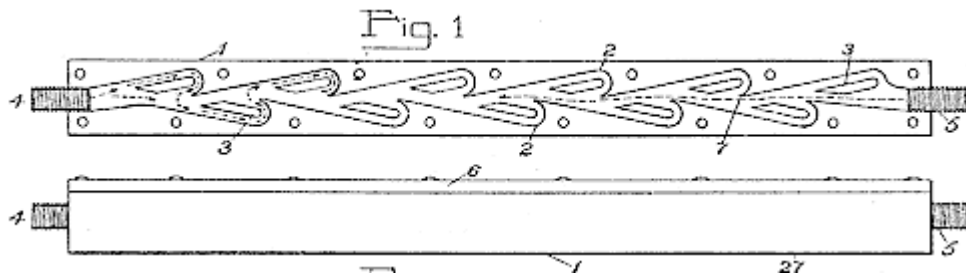
Figure 2.4 Figure 1 from Tesla's valvular conduit patent of 1920 [1]. Forward flow proceeds undisturbed from right to left, but reverse flow is impeded by the curved

Dieter Thoma also patented what he referred to as a fluid line [105]. Similar to the idea of Tesla, the fluid line provides unrestricted flow in one direction and high resistance to flow in the opposite direction. The aerodynamic valve [106] as patented in 1948 proposes a series of nozzles with a diffuser at the end. Once again, this arrangement is designed so that the forward resistance is $1/6^{th}$ to $1/8^{th}$ that of the resistance to flow in the opposite direction.

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Paul [107] analytically and experimentally modeled flow through a one stage momentum diode in order to determine an optimal design for steady state diode resistance. He found that the ratio of reverse to forward flow could be predicted as $X = 1/(1+\lambda)$ where λ is the channel width ratio (main channel width to return channel width). Also, he found the resistance ratios as high as 4.6:1.

The effect of a fluid diode is similar to that of a stenosed valvular conduit. It is an added resistance to the flow. However, in the case of a diode, the stenosis can be designed geometrically to provide a favorable ratio between the forward and reverse flow resistances. The hypothesis of study is that by adding this resistance in the area of the pulmonary valve, that the regurgitation will be less than that of an absent valve.

This idea is further supported by the findings of a study by Kilner et al. [108]. They were interested in how the flow regurgitation varied with different levels of pulmonary arterial compliance and resistance, and the locations of those elements. Using a theoretical model, they found that the free regurgitation was a function of pulmonary compliance and resistance. In regards to resistance, the regurgitant fraction was measured to be 46% (versus a 30% baseline case) when the arteriolar resistance was increased. However, when they increased the pulmonary vascular resistance by simulating pulmonary annular stenosis, the regurgitation dropped to 10%. Since a fluid diode valve in the pulmonary position would essentially be an annular stenosis with low resistance to systolic flow and higher resistance to diastolic flow, the expectation is that the regurgitation would also decrease as compared to an absent valve scenario but

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without the penalty of high systolic pressure gradient corresponding to a high resistance stenosis.

The premise of using a momentum diode valve was tested by Losaw [109]. He studied two diode valve designs as pulmonary heart valve replacements. The first, a nozzle valve, was a benchmark design. The geometry was designed using the long radius nozzle design conventions as outlined in the ASME nozzle design manual, but with a shorter profile [110]. The beta ratio, the ratio of the minor and major orifice diameters, was 0.5. The second valve studied by Losaw was inspired by the Tesla diode. This diode valve incorporated the curved channels similar to the valvular conduit.

The results of the diode valve were compared to that of SJM bileaflet, the nozzle valve and absent valve case. He reported a regurgitation fraction of 15.8± 0.1% for a cardiac output of 5.8 Lpm for the diode valve. This was roughly a 25% improvement over the absent valve case of similar flow rate. The measured transvalvular gradient for the diode valve was 4.2 ±0.6 mmHg, expectedly higher than that of the absent valve. Yet, it is still reasonable. These findings support the idea that a momentum diode could serve as a replacement pulmonary heart valve under certain conditions. Also, it suggests that geometric changes may offer improved results.

Proposed Diode Design

The baseline design is based on the diode valve studied by Losaw [109]. The valve has an elliptical contraction and a backchannel enclosed by an annular ring. The

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cusp of the backchannel has an elliptical profile. The generally dimensioned cross-section is shown in the figure below Figure 2.5.
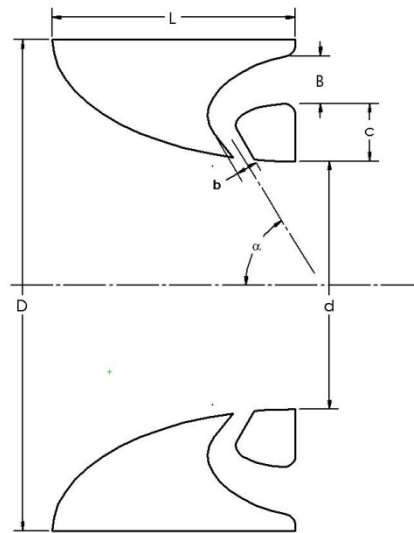
Figure 2.5: Generically Dimensioned Diode Valve

α - impingement angle of backflow channel jet
d – minor orifice diameter
D – major orifice diameter
β - ratio of minor to major orifice diameter, d/D
L – overall length of the diode
b – minor width of backflow channel
B – Major width of backflow channel
c – annular ring width

The concept is that during systole, flow will encounter little resistance from the nozzle type entry. However, during diastole, retrograde flow would be impeded by the smaller diameter and the flow from the backchannels reentering the central flow field and

angle. For the base design, the dimensions are as listed: impingement angle 60°, the β-ratio is 0.5, L is 12.5mm, b is 1.2 mm and B is equal to 2.0 mm. The dimensional variations of this design for other valves that were tested are shown in Table 2.1.

For the sake of manufacturing, a way to simplify the diode design was investigated. The momentum diode valve has a contoured backchannel with an inner ring to enclose it. A solid model rendering of the baseline design is shown in Figure 2.6a. A much simpler design of the momentum diode valve was to eliminate the inner ring or, in terms of the geometric parameters, let c = 0 (see Figure 2.6b). The *open cusped* valve was then made in one piece without the need to machine and hold the inner ring in place.

All diodes were modeled using the 3D CAD software program SolidWorks. The valves that were tested *in vitro* were made by a rapid prototyping machine with an acrylonitrile-butadiene-styrene (ABS) plastic polymer. The valves for PIV testing were replicas of the biological implant. They were made of 316L stainless steel and coated with DLC pyrolitic carbon. The coating was a BioMedFlex® film coating had a thickness of 0.1 - 4 μm, a coefficient of friction of 0.02 – 0.04, and a hardness of 12,000 N/mm^2.
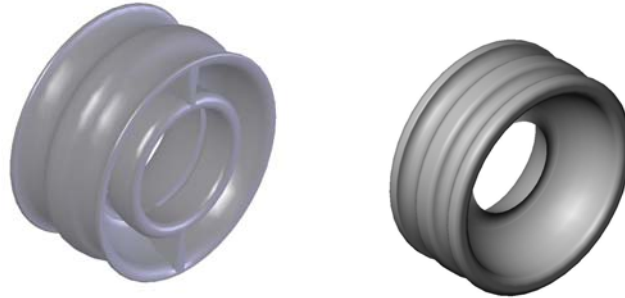
Figure 2.6: Solidworks Models of (a) a diode valve with an enclosed backchannel (backchannel diode); (b) diode valve with an open backchannel (open cusped diode)

Table 2.1: Diode Design Dimensions

Parameter	α	β	L	b	B	c
1 (Baseline)	60	0.50	12.5	1.2	2.0	
2	60	0.50	12.5	Inf	Inf	0
3	75	0.50	12.5	1.2	2.0	
4	75	0.50	12.5	Inf	inf	0
5	90	0.50	12.5	1.2	2.0	
6	90	0.50	12.5	Inf	Inf	0
7	60	0.45	12.5			
8	60	0.40	12.5			

CHAPTER THREE

RESEARCH METHODS

The primary objective of the present study is to test the hypothesis that a motionless momentum diode valve can perform as a replacement pulmonary valve. The review of the literature established that there is a particular need for a replacement valve for patients born with congenital heart defects and suffer from pulmonary insufficiency. Studies also show that the lower operating pressures of the right heart circulation allow for less strict tolerances on pressure gradient and regurgitant fraction. The following strategies will be implemented in order to further evaluate the hypothesis.

The first aim is to test the momentum diode valves *in vitro* over a range of physiological conditions for transvalvular pressure gradients (TVG) and regurgitant fractions (RF%) as functions of pulmonary impedance. They will be compared to traditional replacement valves in the pulmonary position. The criteria for acceptable performance is the ability to regulate flow to moderate and acceptable levels of RF% of (0 - 20% is desired, less than 35% overall) and TVG (0-30 mmHg).

The second aim is to perform a parametric study using geometric variation of the diode valve designs in order to determine how the geometry affects the valve performance. Also, key design parameters that affect flow regulating performance will be identified so that they can later be optimized.

Another objective is to evaluate the diode valve concept *in vivo*. An acute *in vivo* test will be performed in the development of the surgical protocol and technique for the implantation. It will also generate information on how to administer longer term tests. Also, the experiment will produce preliminary information that may answer questions such as: is the data similar to that in the *in vitro* setup? And how will the animal react to the diode valve?

Finally, particle image velocimetry (PIV) will be used to study the hemodynamic performance of different diode designs. Flow field data will be used to evaluate flow patterns, the viscous and turbulent shear stress levels, and estimate the exposure times for a particle (platelet). A threshold level of activation of 35 dynes-s/cm^2 [54] will be used as an upper benchmark for benign activation. The PIV data as a whole will help determine if a momentum diode valve can meet the hemodynamic demands as a prosthetic heart valve.

Mock Pulmonary Circulatory System

A mock circulatory system was used to assess the hemodynamic performance of different diode designs *in vitro*. The system was based on many of the previous designs discussed in the literature review. The mock pulmonary circulatory system (MPCS) modeled the right heart circulation at various physiological settings. It contained open air atrial chambers, ventricle chamber, a pulsatile pump, and compliance and resistance elements. It allowed for pressure and flow measurements to be obtained as well as optical

flow measurements. Figure 3.1 shows a schematic of the MPCS used in the current study.

The right atrium tank was a six (6) inch acrylic tube with one end closed off using a delrin cap. This tank had an overflow connection so that the fluid height in the tank remained constant.

The right ventricle assembly consisted of a balloon enclosed in a chamber. A pneumatic cylinder was connected to the chamber with hosing. The cylinder action was driven by a cam driven pump (Harvard 1423 Pulsatile pump). The amount of stroke that the cylinder encounters was adjusted by changing the stroke volume on the Harvard pump. This pump was designed so that the cycle rate (heart rate, HR) and systolic ratio (SR%) are adjustable.

The test section was made of acrylic and houses the test valve (Figure 3.2). The contraction was constructed to reduce the flow area from 62 mm diameter to 25 mm diameter, the size of the prototype valves to be studied. The profile dimensions were taken from a similar piece done by Figliola [111]. The distal section was modeled after the human pulmonary artery. The internal artery dimensions (Figure 3.3) were scaled for a 25 mm tissue annulus versus the 29 mm that was used by Philpot [79, 80]. The passages were axisymmetric with respect to the flow centerlines.
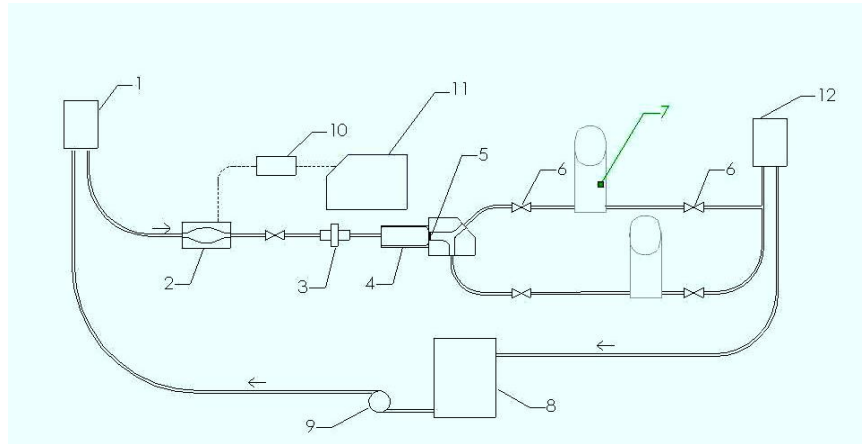
Figure 3.1: Schematic of the mock circulatory system used in this study. Arrows indicate flow direction. 1. Right atrium constant head tank; 2. Right ventricular chamber; 3. Flow meter; 4. Test section 5; Mechanical heart valve; 6. Ball valves; 7. Capacitance chambers; 8. Holding tank; 9. Recirculating pump; 10. Pneumatic cylinder; 11. Harvard Pulsatile pump; 12. Left atrium constant head tank

The resistance and compliance needed to be adjustable in order to test at different physiological states. The compliance in the system was modeled using two Windkessel compliance chambers. They were PVC pipe 4" in diameter and 24" tall and one end is capped. The chambers were positioned vertically, and there was a hose barb tee connection in the end cap through which the blood analog flows. The top end of the chambers were sealed with an inflatable rubber ball plugs so that the amount of trapped air could be varied. This permitted for the adjustment of the tank compliance. The height of the chambers and size of the test plugs allowed for the individual tank compliance to be adjusted up to 4 mL/mmHg.

40
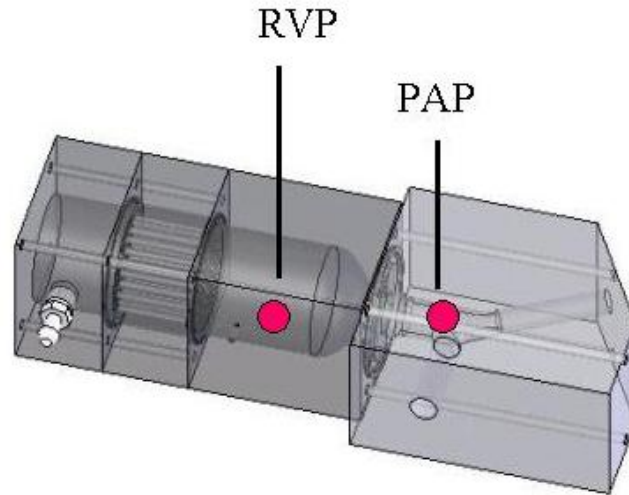
Figure 3.2: Complete test section. RVP and PAP pressure taps shown.
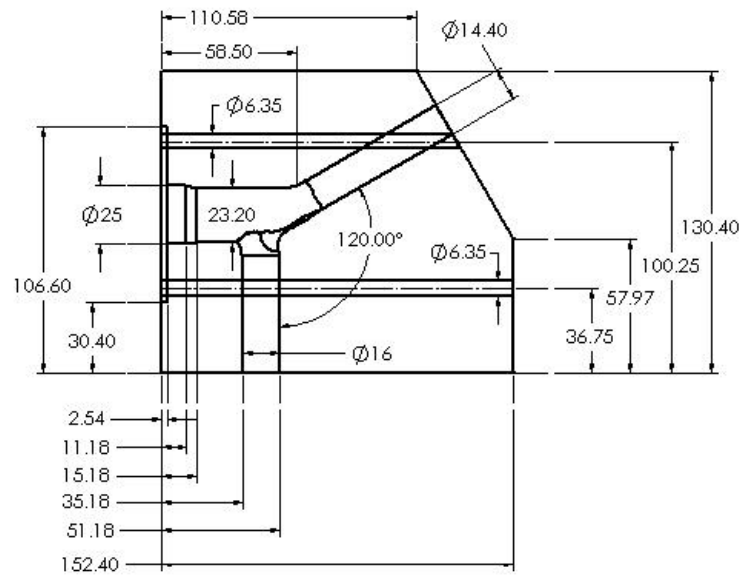
Figure 3.3: Pulmonary artery test section. Dimensions in mm.

In addition to the compliance, the pulmonary vascular resistance of the system needed to be regulated. There was inherent resistance in the system resulting from the tubing and connectors. There were also ball valves that could be used to regulate both the resistance and the flow in each of the arterial branches. The ball valves were located between compliance chambers and the second open air tank that acted as the left atrium. The left atrium tank was designed just like the right atrium tank. It was also used to change the resistance.

<div align="center">Global Flow and Pressure Measurements</div>

The global tests were conducted as a mean of characterizing the hydrodynamic performance of the different valve designs. All data was acquired using an automated data acquisition (DAQ) system controlled by NI Labview[®].

Instantaneous and mean flow data were measured using a Carolina Medical[®] model 501 electromagnetic flowmeter. One probe was attached as shown in Figure 3.1. An additional probe was used to measure flow in one of the pulmonary artery branches. The instantaneous flow readings were separated into forward and reverse flow data by a zero crossing algorithm. Numerical integration was performed on all the flow data to yield the net flow rate through the valve as well as the positive ($Q_{forward}$) and negative flow rates ($Q_{reverse}$) components. Equation 1 shows the simple integration technique used to determine mean flow.

$$Q = \frac{1}{\Delta t} \sum_{i=1}^{n} \frac{(Q_i + Q_{i+1}) \cdot (t_{i+1} - t_i)}{2} \tag{1}$$

The regurgitation fraction was calculated using this data with the following equation:

$$RF[\%] = \frac{Q_{reverse}}{Q_{forward}} \cdot 100 \tag{2}$$

The pressure transducers were BD physiological pressure transducers. The pressure taps were located so that the right ventricular pressure (RVP) and the pulmonary artery pressure (PAP) were measured (Figure 3.2). The transducers were located on a holder fixed to the floor to minimize transmission of system vibrations.

With this information, the transvalvular pressure gradient (TVG), mean pulmonary artery pressure (mPa), pulmonic impedance (PVZ) and pulmonic vascular resistance (PVR), compliance and effective orifice area (EOA) were calculated. Mean pulmonary artery pressure was calculated the same way that the mean flow rate was found. The pressure gradient across the valve was found using equation 3.

$$TVG[mmHg] = RVP_{Peak} - PAP_{Peak} \tag{3}$$

System resistance and compliance were calculated in two manners. To measure the system impedance, a procedure carried out by Gohean, et al. [112] was followed. Fourier analysis was used to transform the time-based signals into frequency domain to obtain a spectrum for both PAP and flow rate (Q) [9, 113-116].

$$Z(\omega) = \frac{|PAP(\omega)|}{|Q(\omega)|} \tag{4}$$

The impedance at the zeroth harmonic (Z_0) is otherwise known as the pulmonary vascular resistance (PVR). Pulmonary vascular compliance can also be extracted from the spectrum data as the first harmonic, Z_1, is shown to be inversely proportional to the system compliance [9].

The second method of calculating PVR and compliance was to use their respective definitions. These approximations are used during data acquisition as a means to estimate the resistance and compliance during system tuning.

$$PVR \left[\frac{mmHg}{L}/min\right] = \frac{mPa}{CO} \tag{6}$$

$$PVC \left[\frac{mL}{mmHg}\right] = \frac{CO}{(PAP_{max} - PAP_{min}) \cdot HR} \cdot 1000 \tag{7}$$

The effective orifice area (EOA) is an index of how well the valve uses its primary orifice area and is another way of gauging how much a valve obstructs flow. It was defined by the following equation for saline [117]:

$$EOA[cm^2] = \frac{Q_{rms}}{51.6\sqrt{\Delta p}}EOA \tag{8}$$

Optical Flow Field Measurements

In addition to global flow data, optical flow field data was collected using PIV. The flow field velocity maps assessed for the thrombogenetic potential of each valve by magnitude of stress, stress exposure times, and areas of stasis.

Particle Image Velocimetry

Particle image velocimetry (PIV) is a noninvasive method of measuring velocity. It provides and indirect fluid flow measurement and also allows for whole flow fields to be captured. Typically, an experimental setup of a PIV system has several subsystems. Tracer particles are added to the flow. They are illuminated in a plane by a light sheet by means of a laser. This happens at least twice within a short, known time interval and the light scattered by the particles is recorded with a high quality lens of two separate frames on a cross correlation CCD sensor. The images are stored directly on a computer and are evaluated in order to determine the displacement of the particle images. This is done by dividing the PIV recordings into small sub-areas called "interrogation areas". For each interrogation area, the displacement vector for the particles is found by means of auto and cross-correlation methods [118].

There are some considerations that need to be taken into account when setting up the PIV system. One issue is that of velocity lag and therefore particle size. Tracer particles should follow the motion of the fluid elements. Small particles will follow flow better. Light source power is another area to consider. While high gas flows may require a high power light source in order to get light scatter off of small tracer particles, liquid flows can tolerate larger particles. These scatter more light; therefore, a lower peak power laser can be used. The duration of the illumination pulse should be short enough to 'freeze' the particle motion; thus, no streaks or blurry images. The time delay between pulses should be long enough for the particles to have detectable displacement, but short

enough to avoid particles leaving the plane of the light sheet. The tracer particles should be distributed homogenously at medium density so that you cannot detect any flow field structures [118].

For this study a dual pulsed Gemini PIV Nd:Yad laser (New Wave Research, Inc., Fremont, CA) was used to created a 1 mm thick laser sheet for illuminating particles. A FlowMaster 2S LaVision CCD camera along with DaVis v6.2 software was used to capture images. The particles used were 10 μm silver coated hollow glass spheres. An output switch on the Harvard Pulsatile pump signaled the start of systole for each pulsatile cycle. It was connected to a BNC Model 555 Pulse/Delay generator in order to trigger the camera externally. The pulse generator allowed for the trigger to be delayed throughout the cardiac cycle in order to fire the camera and laser at known times. Twenty-five (25) image pairs were collected at 50 ms time intervals over the course of a cycle.

The laser sheets were arranged so that flow fields parallel to the branch plane were analyzed. In order to do this, the camera was placed in an overhead position. It was mounted to a traversing mechanism that allowed for it to be moved in all three directions. The laser and mirrors were positioned as shown in Figure 3.4.

The laser slit was on a track so that it, and thusly the laser sheet, could be moved to different vertical positions along the test section. The planes of view that were of

interest are shown in Figure 3.5. Data was collected in three planes. One along the centerline and two offsets 4 mm above and below the center.

In order to get accurate velocity vectors from the PIV cross-correlation, a pixel calibration procedure was carried out. This was done by placing a scale of known length in the view of the camera. In the 'Camera Scales' option in DaVis, a known distance was selected and entered. This associated a distance in millimeters to each pixel. For the PIV data collected, the pixel calibration was 22.7 mm/pixel.
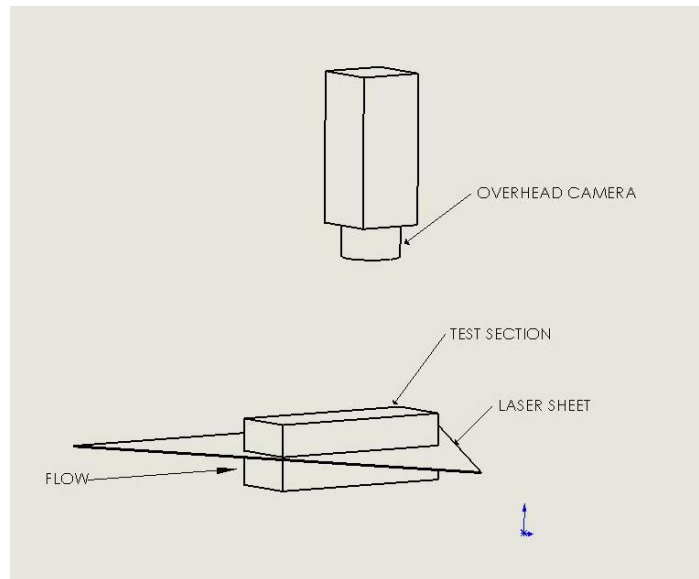
Figure 3.4: PIV setup

The software DaVis was used to both collect and analyze the PIV data; thus, both the laser and the camera were connected to the PIV data acquisition card as instructed by

the DaVis catalog. The laser and camera triggering were operated by the software. However, the timing needed to be externally controlled so that images could be acquired at a known point in the cardiac cycle. A switch output from the Harvard pulsatile pump was connected to the pulse generator as a trigger. The pulse generator accepted this trigger and then output a TTL signal to the DaVis card. This output could be delayed from the initial trigger by any time. In this case, the delays were from $0 - 750$ ms in 50 ms increments.
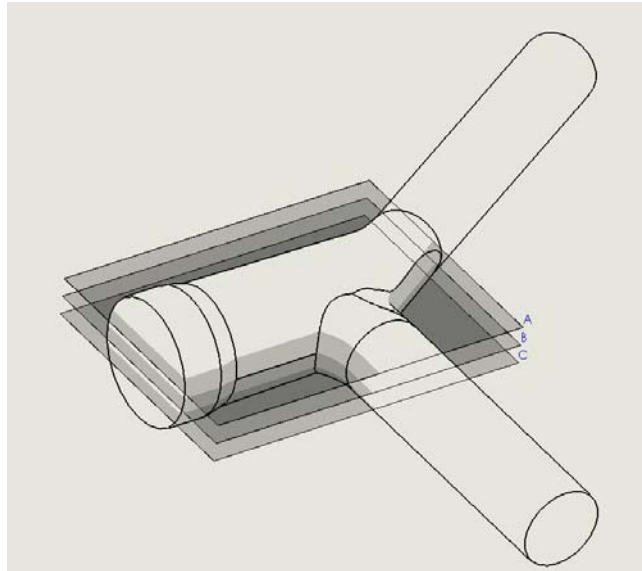
Figure 3.5: Flow Field Planes that will be analyzed with PIV

The images were captured and stored using the 'Sequence' command. At each time step, twenty-five images were collected. The files were named so that it identified

the time step, the plane of view and the PVR level to which the system is tuned.

The 'Image Processing' command was used to batch process the 25 image pairs. Each image pair was analyzed using a double pass cross-correlation scheme with an initial interrogation window of 64x64 pixels and a final interrogation window of 32x32 pixels. The second pass was offset. A peak velocity filter of 2 – 4 m/s was employed based on expected maximum velocities. A mask file was created to block the regions of the images that were not within the flow field. An ensemble average of these images was found using the algorithm in DaVis. Each individual (from each image pair) and mean file was saved as a text file with the results from DaVis cross-correlation. The text files included the x and y positions, u, the velocity in the x direction and v, the velocity in the y direction.   The mean data files contained the same data with the mean velocity components,$\bar{u}\ and\ \bar{v}$ instead of the instantaneous velocities. The variable n represents the number of cycles.

$$\bar{u} = \textstyle\sum_{i=1}^{n} u_i \tag{9}$$

$$\bar{v} = \textstyle\sum_{i=1}^{n} v_i \tag{10}$$

This data was then further analyzed using in house algorithm written in Matlab. The viscous shear stresses were calculated using shearing strain rate based on the time-averaged flow velocities, $\bar{u}, \bar{v}$, of twenty five cycles as described in equation 11. The number of image pairs, N, was chose based on the convergence of u_{rms} as N was increased. The values for u_{rms} and N are shown in

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Table 3.1 for tested open cusped diode tested at PVR = 3.1 mmHg/Lpm. The values were chosen at the same location in the flow field as the N increased. Various points in the flow field were compared and trended similarly. The rms value of the x-component of the velocity asymptotically approached 0.400 beginning at N= 25.

Table 3.1. The Root Mean Squared of the velocity components for increasing number of image pairs.

N	u_{rms}
5	0.6325
10	0.5256
15	0.4573
20	0.4253
25	0.4001
30	0.3960
35	0.3980

$$\tau_{xy} = \mu \left(\frac{d\bar{u}}{dy} + \frac{d\bar{v}}{dx} \right) \tag{11}$$

The derivatives were calculated with a central difference method. At the walls, when data was only available in one direction, forward and backward difference methods were used to approximate the strain rate.

The velocity fluctuations, u' and v', and were found by taking the difference between the time-averaged mean velocity and the instantaneous velocity as shown in equations 12 and 13.

$$u' = u - \bar{u} \tag{12}$$

$$v' = v - \bar{v} \tag{13}$$

The Reynolds shear and normal stresses were found with equations 14 -16. For each cycle, the product of the velocity fluctuations was found. These products were then averaged in order to yield the turbulent shear stress as showing in equation 14. The turbulent normal stresses were found in a similar manner.

$$\tau'_{xy} = -\overline{\rho u'v'} \tag{14}$$

$$\tau'_{xx} = \overline{\rho u'u'} \tag{15}$$

$$\tau'_{yy} = \overline{\rho v'v'} \tag{16}$$

Finally, the turbulence intensities were found with the following expressions:

$$u_{rms} = \sqrt{\frac{\sum_{i=1}^{n} \overline{u'^2}}{n}} \tag{17}$$

$$v_{rms} = \sqrt{\frac{\sum_{i=1}^{n} \overline{v'^2}}{n}} \tag{18}$$

All stress values are reported with units of dynes/cm^2.

Laser Doppler Velocimetry Measurements

Laser Doppler velocimetry (LDV) is a method used to measure velocities at a point. It is best used to characterize local turbulent properties as a result of its high

temporal and spatial resolution. The LDV system used here was a TSI® computer-controlled, two-component fiber optic system with dual Bragg-cells, digital spectral flow analyzer, and a multiband 6W Spectra-physics Stabilite argon-ion laser source. The laser head was placed on a traversing mechanism that moved in the x, y and z directions so that the beam could be positioned anywhere in the flow. The system provided two-dimensional velocity component information with both forward and reverse flow measuring capability. The LDV setup is shown in Figure 3.6. LDV measurements were collected in the areas of elevated Reynolds shear stresses that were identified by the PIV measurements and the power spectrums were calculated.

The data was initially sorted by grid location. Then, the 12,000 points were divided into different cycles. Any cycles containing more than 900 data points were omitted. This was to maintain Zeros were appended to any cycles with less than 900 points so that each cycle had an equal same number of cycles. The data was then written out into a column of data for each cycle. So, instead of a column array of 12000 points, there were 12 columns of approximately 890 points.
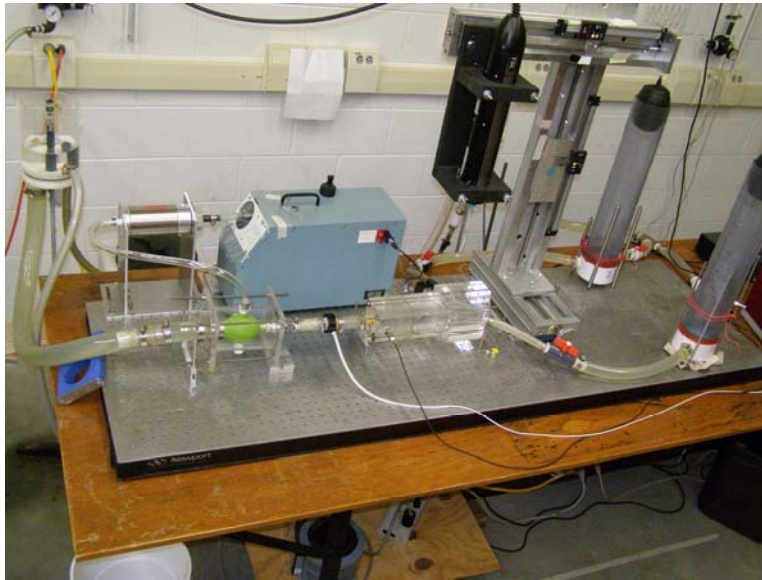
Figure 3.6: LDV setup

A second analysis sorted data from the initial program and calculated the average over the cycle. A quasi steady condition was assumed for the pulsatile cycle over 10 data points. Therefore, the cycles were divided into 89 periods of 10 points each and the average values for these over all the cycles were determined. The velocity fluctuations, u' and v', were found for each point in the cycle by subtracting the mean value from the velocity component.

In the final phase of the analysis, the fast Fourier Transform (FFT) was performed on the data. The FFT was done on the autocorrelation of the both the axial and radial velocity components. Then, the ensemble average was calculated. The order of the operations was changed (ensemble average, then FFT) without any differing effect. A 100 point discrete Fourier transform (DFT) is designated. The magnitude of each

complex value was found, and the frequency was normalized from 0 - 500 Hz. A basic moving average smoothing function with a window size of 3-5 points was applied to the final magnitude curves.

<div align="center">Test Fluids</div>

The blood analog solution for global testing and measurements was a 40% by volume glycerin/water solution. Sodium chloride was added in order to provide a charge for the electromagnetic flow meter. The kinematic viscosity was checked using a Cannon-Fiske U-tube viscometer and the specific gravity with a hydrometer. The solution typically had a viscosity of 3.25 cSt and a specific gravity of 1.095. For optical studies, the refractive index of the blood analog needed to match that of the acrylic test section in order to minimize distortion. Therefore, a solution of 79% saturated sodium iodide, 20% glycerin and 1% water. The resulting solution had a refractive index ranging from 1.46 - 1.49, a kinematic viscosity similar to that previously stated, and specific gravity of 1.6. Both solutions were mixed by using a scale to measure out the appropriate percentage of components and mixed thoroughly. Since kinematic similitude was held, the Reynolds number for all the testing with glycerin/water solution as well as the glycerin/water/sodium iodide solution was the same. For all tests, Re was on average 1407 for flow rates of 5 Lpm with maximum values reaching 7037 for flow rates of 25 Lpm.

CHAPTER FOUR

DIODE PERFORMANCE TESTING RESULTS

Preliminary Testing

The first two criteria that the diode valves must meet in order to be considered for a pulmonary valve replacement are regulating flow so that the regurgitant flow less than 35% and the transvalvular gradient is less than 25 mm Hg. As a preliminary study, the performance of the diode valves were compared to that of the mechanical heart valves commonly used as pulmonary heart valves. The mock pulmonary circulatory system was used to test all the valves.

MPCS Variations

The ventricle in the preliminary tests was driven by compressed air regulated with a system of pneumatic solenoid valves instead of the Harvard pulsatile pump. The valve timing was controlled using a BNC pulse generator. The stroke volume of the ventricle was maintained by adjusting a needle flow control valve on the inlet hose that lead to the ventricle chamber. Also, an alternate style of compliance chambers was used during these tests. These chambers consisted of a rubber hose housed in a 4" diameter acrylic tube. The chamber could be pressurized using a pressure bulb and vented in order to adjust the resistance and compliance of the system. The pressure transducers used were Druck LPM 5480 in lieu of the BD physiological transducers.

Test Conditions

For these tests, the following conditions were maintained: cardiac output of 5 Lpm, pulse rate of 75 beats per minute (bpm), and a systolic ratio of 45%. The PVR was then varied between 1 and 5 mm Hg/Lpm. This was done by changing the downstream resistance by adjusting the ball valves, the height of the left atrial tank, and the stroke volume of the pump. The system compliance is coupled with the system resistance and was held between 2 ml/ mm Hg and 6 ml/mm Hg for these set of tests.

The baseline diode valve design was tested alongside a St. Jude Mechanical bileaflet valve (SJMBV) and the MedicalCV Omnicarbon tilting disk valve (OTD). Each valve was tested in the MPCS over a range pulmonary vascular resistance. These results have been previously reported in Camp et al. [119].

Diode to Mechanical Heart Valve Comparison

Pressure and Flow Curves

The right ventricular pressure, pulmonary artery pressure and flow rate signals were obtained for each type of valve. Figure 4.1 and Figure 4.2 are the traces for the SJMBV and OTD valve. In general, the pressure and flow signals are consistent with physiological traces [12]. The PAP curve for each displays a clear dicrotic notch at the point of valve closure. At this point, the flow rate in both cases shows some valve regurgitation or retrograde flow. The flow rate curve oscillates a little around the zero, indicating leakage through the valves. The RF% for both the OTD valve and the SJMBV

are on the same order. The transvalvular gradient for each mechanical valve is less than 5 mmHg.

The pressure and flow traces for the momentum diode valve is shown in Figure 4.3. The curves are well correlated. Yet, there a notable difference between the diode and the MHVs curves. There is no clear dicrotic notch because valve closure never occurs. Therefore, the diastolic PAP gradually approaches the diastolic RVP. Also, there is a sustained level of regurgitant during diastole.
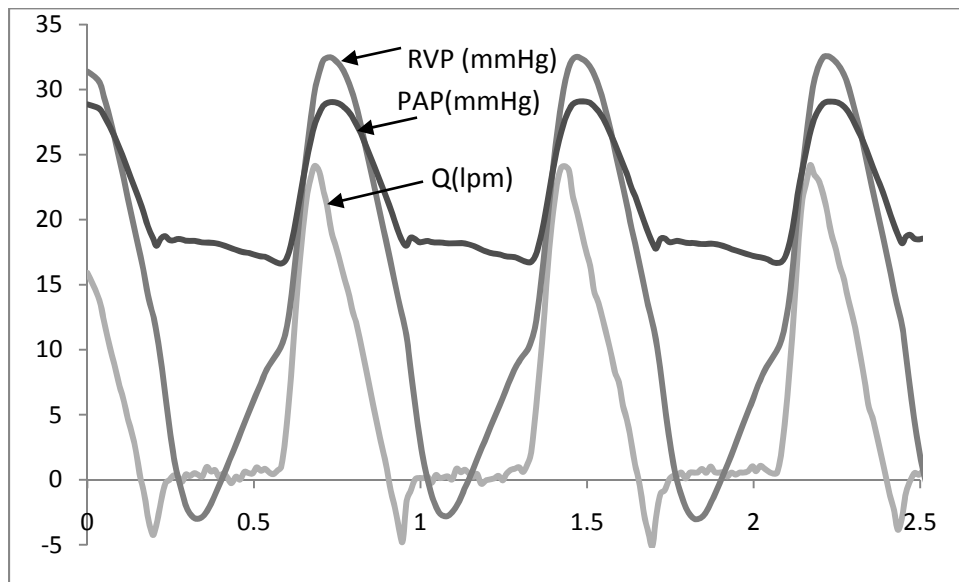
Figure 4.1: Physiological signals using SJMBV (5 Lpm, 75 bpm, 3.9 mm Hg/Lpm)

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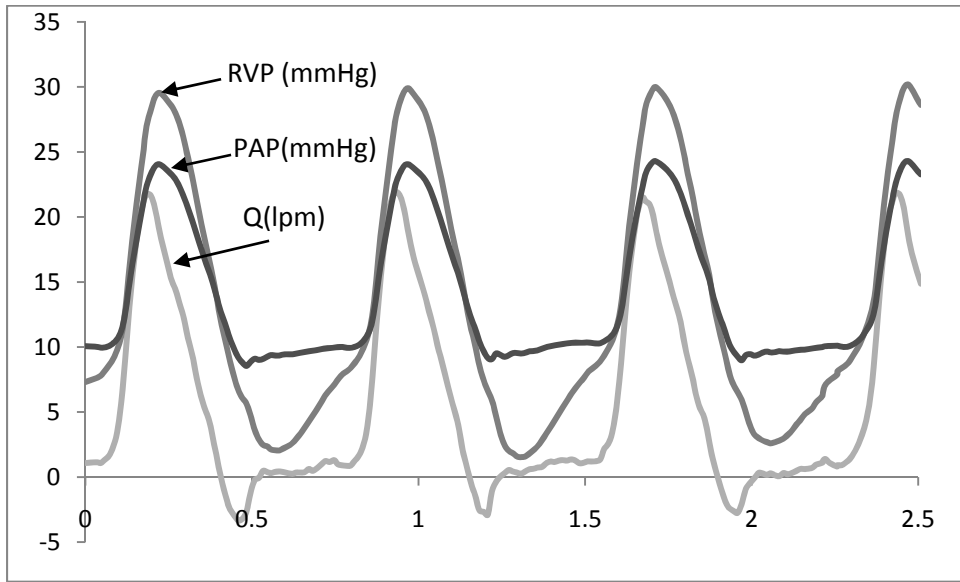
Figure 4.2: Physiological signals using OTDV (5 Lpm, 75 bpm, 2.9 mm Hg/Lpm)
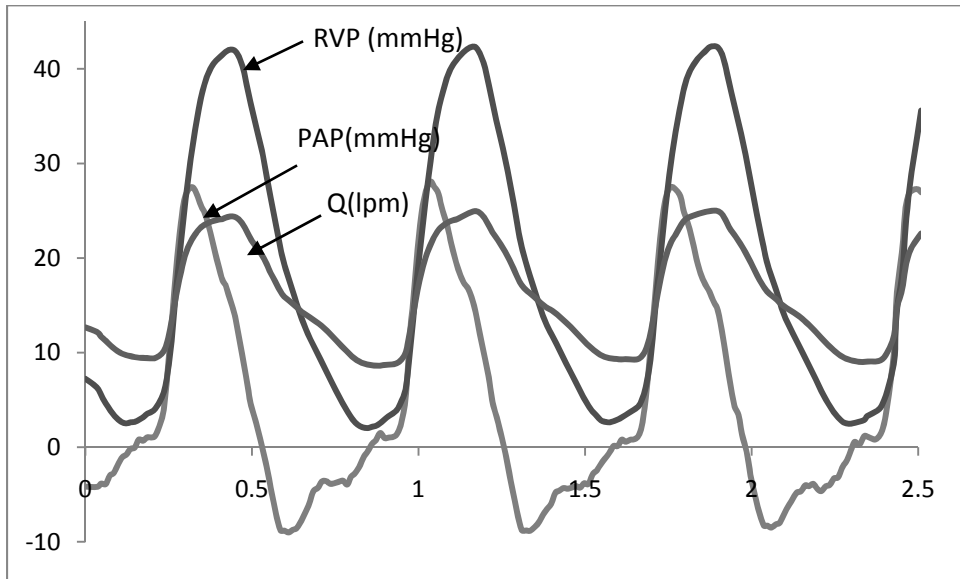
Figure 4.3: Physiological signals using diode (5 Lpm, 74 bpm, 3.1 mm Hg/Lpm)

Performance Data

Each valve was tested at different levels of PVR. The regurgitant fraction and pressure gradient were calculated for each case using equations 2 and 3. The effective orifice area was also found (Equation 8). Figure 4.4 summarizes all the RF% and TVG data. The EOA calculations are listed in Table 4.1.
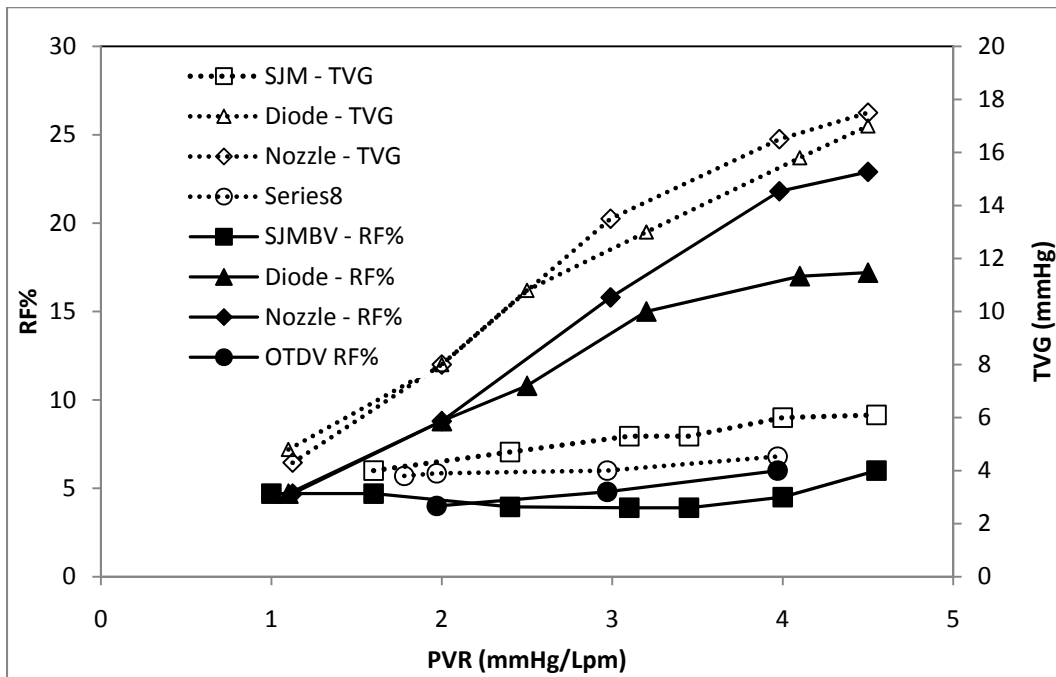
Figure 4.4: Regurgitant Fraction (RF) and peak to peak transvalvular gradient at 5 Lpm

Table 4.1: Summary of effective orifice area (5 Lpm and 75 bpm)

	Cardiac Output (Lpm)	PVR (mm Hg/Lpm)	EOA (cm^2)
SJMBV	5.1 ± 0.1	3.05 ± 0.1	3.64
OTD Valve	5.2 ± 0.1	2.9 ± 0.1	2.45
Diode	5.1 ± 0.1	3.0 ± 0.1	1.24
Nozzle	5.1 ± 0.2	3.0 ± 0.1	1.13

The regurgitant fraction and transvalvular gradient for the SJMBV and OTD valve do not appear a function of the PVR. The RF% for the bileaflet valve ranges from 4% - 6% and between 6% and 7% for the tilting disk valve. As reported by Gohean et al. [40], the leaflets of the SJMBV do not fully close at PVR values less than 2 mm Hg/Lpm and the OTD valve does not close at PVR below 1.6 mm Hg/Lpm. However, the associated changes in RF% at low PVR are not significantly different ($p < 0.025$). While these valves do not experience complete closure, the regurgitant flow is low because the diastolic pressure gradients are too low to drive significant retrograde flow. The TVG also does appear to be sensitive to PVR. It ranged between 4 to 7 mm Hg for the mechanical valves. The EOA was 3.64 cm^2 for the SJMBV and 2.45 for the OTD valve. This was slightly lower than reported for similar valves in the aortic position [71, 120]. The uncertainties in the RF% values were estimated at $\pm$ 0.5% and the TVG values are $\pm$ 0.4 mmHg at 95% confidence for either valve.

The performances of the diode and nozzle valves are sensitive to PVR. With the diode, the RF% values range from 2% at 0.9 mmHg/Lpm to 17.2% at 4.5 mmHg/Lpm. This is significant ($p < 0.025$) improvement over the flow nozzle for values of PVR > 2.0 mmHg/Lpm. For values below 2.0 mmHg/Lpm, the diode and nozzle both compare well with the MHVs. For the diode valve, the pressure gradient increases with PVR reaching a magnitude of 17 mmHg. The differences between the diode and nozzle gradients are not significant ($p < 0.025$). The EOA for the diode is improved over that of the nozzle. Both motionless devices compare favorably with the performance of some competent

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mechanical and bioprosthetic valve in the aortic position [71, 120]. Uncertainties in the RF% values were estimated at ±1.2% and TVG values at ±0.7 mmHg at 95% confidence for the motionless devices.

Despite the identical central flow areas of both the diode valve and the nozzle, the diode valve showed more forward flow and less regurgitant flow than the nozzle for a given setting of the MPCS. The implication is that regurgitant flow can be reduced by diode design, such as by use of the backchannel diode. The diode design increases resistance to backflow. The enhanced forward flow is likely due to forward flow expanding into the channels over slightly less resistance in the forward direction.

Summary

The results of this study continue to support the idea that a motionless momentum diode valve can be used to regulate flow in the pulmonary position. The diode valve showed improvement in ability over the flow nozzle to impede regurgitant flow. For a PVR range of 1 to 5 mmHg/Lpm, the diode valve yielded a RF% of 2% to 17% as compared to the 2% to 23% for the nozzle. Both valves had TVG values up to 17 mmHg.

CHAPTER FIVE

ANIMAL MODEL RESULTS

Introduction

In this portion of the study, the fluid diode valve was tested in a swine model in order to compare the pressure gradients and regurgitant fractions. The objectives of the acute non-survival animal model were to develop implantation and surgical strategies, to assess the immediate tolerance and eliminate catastrophic response to diode implantation, and to obtain *in vivo* physiological data to validate *in vitro* test results.

Methods

In vitro system setup

Valve tests were conducted in the mock circulatory system (MCS) as described in chapter 3. For these tests, conditions were maintained at a nominal cardiac output of 5 Lpm at a pulse rate of 110 bpm and systolic ratio of 40% [5] for comparison with the *in vivo* studies. The pulmonary vascular resistance was varied between 1 to 4.5 mm Hg/Lpm. This change was done by adjusting the downstream resistance to increase the mean pulmonary artery pressure while maintaining flow rate and pulse rate.

Valve designs

The diode valve design studied was an open cusped diode with a 60˚ impingement angle (design 2 in Table 2.1). The diode has groves on the outer diameter that act as suture rings. These can be seen in Figure 2.6. The biological implant was constructed of

316L stainless steel and was coated with a carbon thin film coating. The BioMedFlex® film coating is a proven coating that has been used in medical blood flow devices requiring a nonthrombogenic surface.

Animals and operative procedures

Structural integrity, anti-thrombogenicity/anti-calcification, implantation techniques, and hemodynamic performance of the diode in a biological milieu were tested. A 70 kg farm swine was adopted due to similarities to humans in the coagulation cascade, platelet function, and platelet-leuckocyte-enthothelial cell interaction. These make pig models more suitable for analyzing thrombosis and platelet activation resulting from prosthetic valves [121]. Following general endotracheal anesthesia, a full median sternotomy was performed, and the heart suspended in a pericardial well. Cardiopulmonary bypass cannulas were placed into the ascending aorta, and directly into both superior and inferior vena cavae. After systemic heparin anticoagulation was achieved, as demonstrated by an activated clotting time > 400 seconds, the animal was placed on complete cardiopulmonary bypass. The main pulmonary artery was opened, and the native pulmonary valve excised.

A test valve was pre-implanted in a Gore-Tex vascular graft. This graft was then sutured into the pulmonary artery. The patient was weaned off by-pass. Pressure catheters were implanted and a flow probe placed around the PA. Data were recorded for up to two hours. Following euthanasia, the valve was retrieved and analyzed for platelet deposition and the lungs and heart examined.

Measurements

In the *in vitro* system, measurements were collected as described in the Research Methods section. However, the pressures were measured using AD Instruments physiological transducers with a Measurements Group 2120 amplifier instead of BD DTXPlus physiological pressure transducers and the in house amplifier. For the animal model, BD DTXPlus transducers were also used with a portable Omega Omni AMP III amplifier to measure pressure. NI Labview® was used in both instances to record the data. The valve performance was evaluated by determining the RF% and PPG as given in Equations 2 and 3.

Results

Prior to surgery, the diode valve was mounted into Gore-Tex graft. The entire vessel was successfully implanted and the patient was weaned off by-pass. The 25 mm valve was oversized for the patient's 18 mm artery. This clearly affected outflow from valve. Data collected for two hours. Over this period, dopamine was used to manipulate vascular parameters.

Table 5.1 summarizes the RF% and TVG from select cases during the third animal trial. The administration of dopamine resulted in an increase of pulmonary vascular resistance from 2.4 to 6.3 mmHg/Lpm. The RF% was thereby increased from under 22% to 46.4%. The increase of PVR also caused the cardiac output to decrease. This was more than likely a result of a constant stroke volume of the heart coupled with the increase in RF%; thus, the net flow rate dropped.

Table 5.1. Select Results from the Animal Model Testing with 95% Confidence Intervals

HR (bpm)	CO (Lpm)	PVR (mmHg/Lpm)	Compliance (ml/mmHg)	RF%	TVG (mmHg)
158	6.2 ± 0.07	2.1 ± 0.04	2.2 ± 0.08	11.3 ± 0.70	10.9 ± 2.86
161	6.2 ± 0.17	2.4 ± 0.07	2.3 ± 0.20	15.1 ± 1.35	13.9 ± 2.55
130	*4.6 ± 0.15*	*2.4 ± 0.09*	*3.1 ± 0.1*	*21.9 ± 1.4*	*21.2 ± 3.18*
123	*2.7 ± 0.31*	*6.3 ± 0.08*	*1.0 ± 0.1*	*46.4 ± 6.09*	*22.7 ± 4.08*

A representative flow and pressure curve from the animal study is shown in Figure 5.1. The curve generated by the MPCS is comparable to figure shown. There is a diastolic pressure gradient of about 10 mmHg. The PVR was 4.4 mmHg/Lpm, a PVC of 2.2 mL/mmHg, and the flow ranged from 15 Lpm to - 8 Lpm giving way for a RF% of 29%.

The resulting regurgitant fractions and transvalvular gradient as a function of PVR for both the *in vitro* and *in vivo* studies are shown in Figure 5.2 and Figure 5.3. The RF% for the *in vivo* tests levels off around 30% for high values of PVR. The *in vitro* curve shows a similar trend. The RF% is held to moderate levels of less than 30% for resistances below 3 mmHg/Lpm.

The pressure gradients are higher for the animal models than those measured in the mock circulatory system. The differences are more noticeable at resistances above 2 mmHg/Lpm. This variance may be a result of the change in compliance noted at each these points. Also, the locations of the pressure catheters could not be replicated in the animal model and this could affect the pressure measurements.
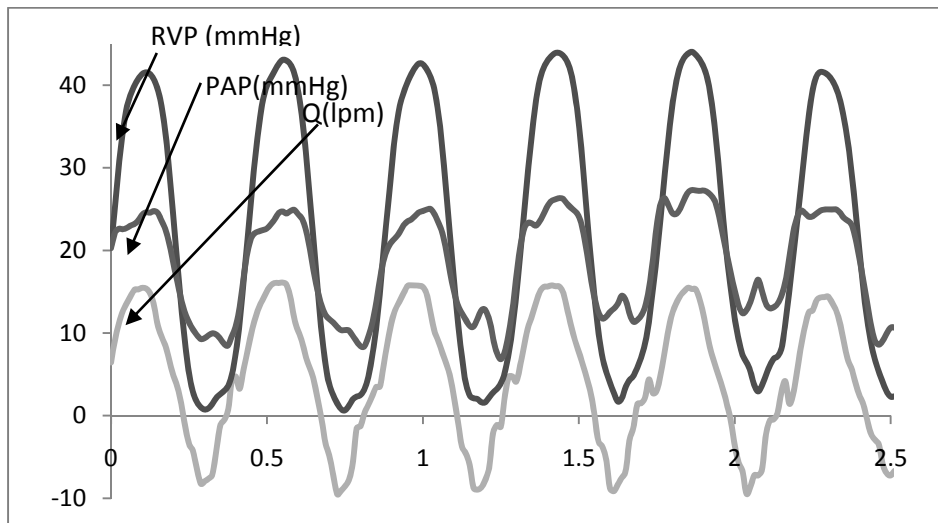
Figure 5.1. Example flow and pressure curve collected during animal tests
using a 25 mm opencusped diode valve

In both models, there is relationship between the pulmonary vascular resistance and pulmonary vascular compliance. The PVC is shown to decrease as PVR increased. The curves for both systems are shown in Figure 5.4. Separation is seen at PVR values below 2.5 mmHg/Lpm.

Summary

The acute animal model demonstrated no catastrophic effects of using a motionless pulmonary valve. The patient was weaned successfully off by-pass. Valuable lessons regarding pharmacology were learned. An implantation strategy was developed that can be carried into a chronic test animal model. *In vivo* performance results are consistent in both tendency and magnitude with *in vitro* findings. Under normal values of compliance (2 to 3 mL/mmHg) and pulmonary vascular resistance (2.3 to 3 mmHg/Lpm),

regurgitant fraction and transvalvular gradients remain within levels known to be well tolerated in humans. Under the influence of dopamine, the vascular resistance was increased to over 6 mmHg/Lpm and compliance decreased to 1 mL/mmHg, resulting in increased levels of regurgitant fraction and higher gradients. However, a compromising factor in these tests was a valve size to patient mismatch, which likely altered valve flow into the pulmonary artery.
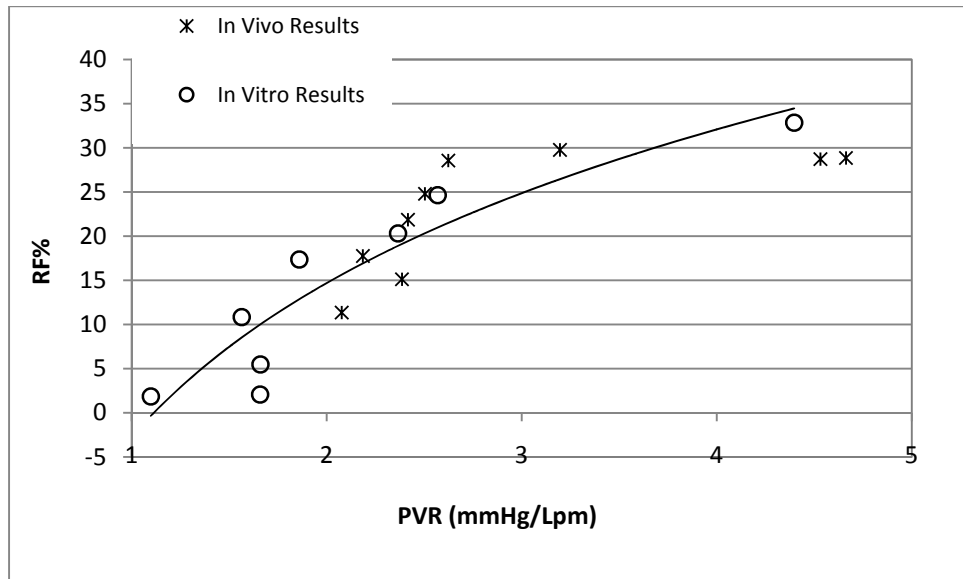
Figure 5.2. PVR vs RF% for both the in vivo and in vitro tests. In vitro test completed at 110 bpm, CO = 5 Lpm.
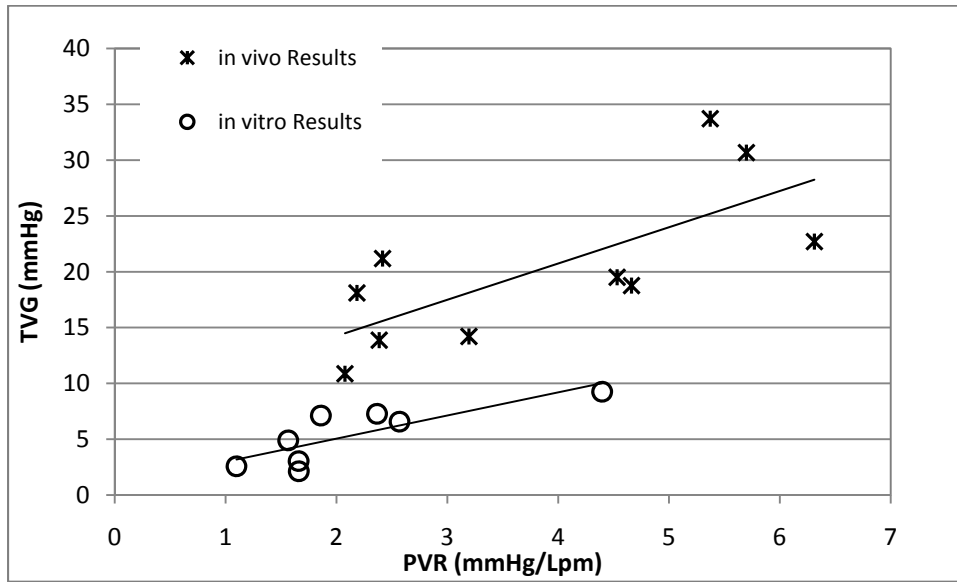
Figure 5.3. TVG vs RF% for both the in vivo and in vitro tests. In vitro test completed at 110 bpm, CO = 5 Lpm.
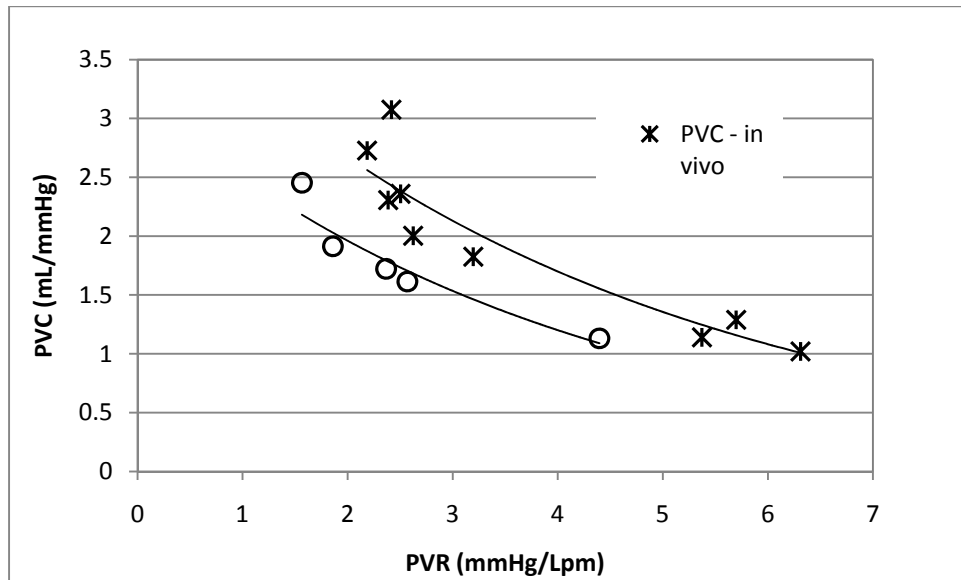
Figure 5.4. PVR vs PVC for animal model and the in vitro model with a 25 mm open cusped diode valve.

CHAPTER SIX

PARAMETRIC STUDY RESULTS

There were two sets of comparison tests. The first study compared the baseline diode design to designs 2 - 6 that had varying impingement angles and inner ring configurations (Table 2.1). The second set of tests compared three valves with different beta ratios (inner orifice diameters). The designs, 1, 7 and 8, are also listed in Table 2.1.

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Test conditions

All the diode valves were tested in vitro in the MPCS as described in Chapter 3. The system was tuned so that the pulmonary vascular resistance was varied between 1.5 and 6.5 mmHg/Lpm. For the first tests, the cardiac output was maintained at 5 Lpm. For the beta ratio test, the cardiac output was maintained at 4 Lpm. This decrease in flow rate was necessary to ensure that a maintaining a constant flow rate would be achievable over a range of PVR levels. The heart rate for all tests was held at 75 bpm.

The operating values of pulmonary vascular resistance and compliance reported are determined based on the spectral method of Gohean et al. (2005) using the instantaneous flow rate and pressure signals, but nominal values were set based on observed pressure and flow traces. A characteristic compliance – resistance curve of the system is given in Figure 6.1 for a system containing a 25 mm open cusp diode valve using blood analog. The system is adjustable over the range of pulmonary vascular

resistance (PVR) of 0.5 to 6 woods and a pulmonary vascular compliance of between 6 to 1 mL/mm Hg. The PVR was changed in this work by increasing flow resistance downstream of the Windkessel compliances.
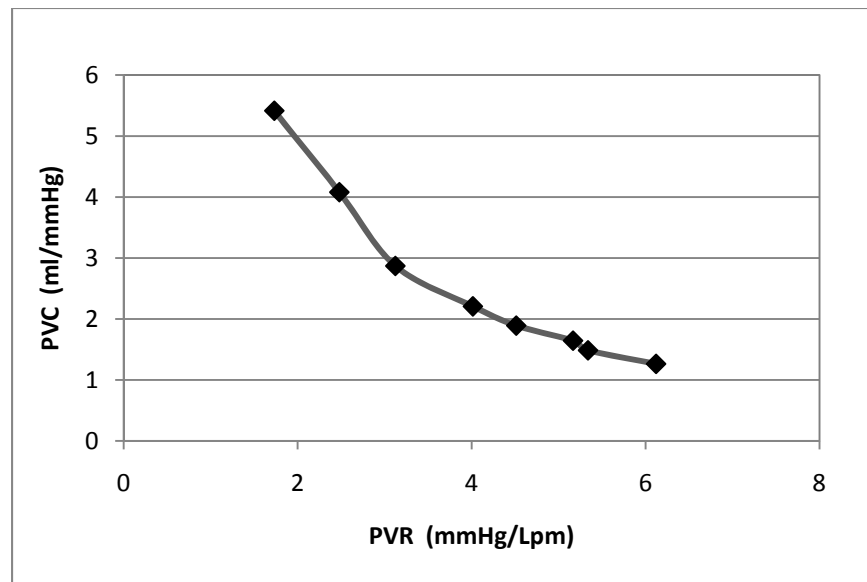
Figure 6.1. Characteristic Resistance - Compliance Curve for an Open Cusped Diode Valve

Results – Varying α and Inner Ring

The six diodes with different impingement angles and cusp designs were tested at similar pulmonary vascular resistances. The goals of PVR = 2.5, 3.5, 4.5 and 5.5 mmHg/Lpm were targeted. The resulting PVR varied as did the cardiac output. For each setting, data was sampled for 120 seconds (150 cycles). Three replications of each data point were recorded. The cardiac output and PVR was averaged for the three points and

the 95% confidence interval was calculated for each. The overall cardiac output for all tests was 5.05 ± 0.3 Lpm. The resulting regurgitant fractions and transvalvular gradients were also averaged and reported with their 95% confidence intervals.

Figure 6.2 shows the both the RF% and pressure gradient as a function of PVR for each backchannel diode. This illustrates any influence that the impingement angle may have on the performance for the backchannel valve. The pressure gradient increases with increasing PVR for all the valves shown. This is expected as the increase in upstream pressure must increase to drive the flow needed to maintain a constant cardiac output. The overall TVG values range from 9.38 ± 0.05 to 22.5 ± 0.318 mmHg. Since the PVRs are not exactly the same for each valve, point to point comparisons are not truly valid. The results do imply that the differences between the TVG curves are not significant (p-value < 0.025). No valve shows more than a 10% improvement over another. The impingement angle was not expected to have a great influence on the pressure gradient.

The regurgitant fraction data points in Figure 6.2 also show that the RF% to be a function of PVR. There is some separation between the curves in these results. At the PVR levels between 2.4 and 2.6 mmHg, the backchannel diode with a 60˚ has a RF% that is significantly lower RF% than the other valves with a 21% difference. As PVR was increases, the improvement decreases. The valve with 75˚ impingement angle seems to have a lower RF% than that with a 90˚ angle at lower resistances.

The open cusped diode valves are compared in Figure 6.3. The difference between the behaviors of these valves is more pronounced than with the backchannel diodes. The transvalvular gradient for the 60˚ open cusped valve is 30-35% higher than that of the other two valves at some points. As PVR increases, the pressure gradient curve for the 60˚ valve becomes less sensitive to PVR. The pressure gradients range from 16.7 to 27.4 mmHg for PVRs between 2.6 to 5.3 mmHg/Lpm. The 75˚ valve has the lowest TVG for all resistances of the three valves for point at PVR less than 5.5mmHg/Lpm with differences between the 75˚ and 90˚ being as high as 13%.

The RF% for all open cusped diode valves for a range of PVR is also shown in Figure 6.3. Overall, the order of the regurgitant fraction curves follows that of the pressure gradients. For resistance levels higher than 3.5 mmHg/Lpm, the 75˚ valve has the lower RF%, the 90˚ valve is in the middle, and the 60˚ has the highest. The regurgitant fraction percentages for the 60˚ valve were measured between 18 and 40%. At the endpoints the uncertainties make it such that the difference between the valve regurgitant fractions is not significant.
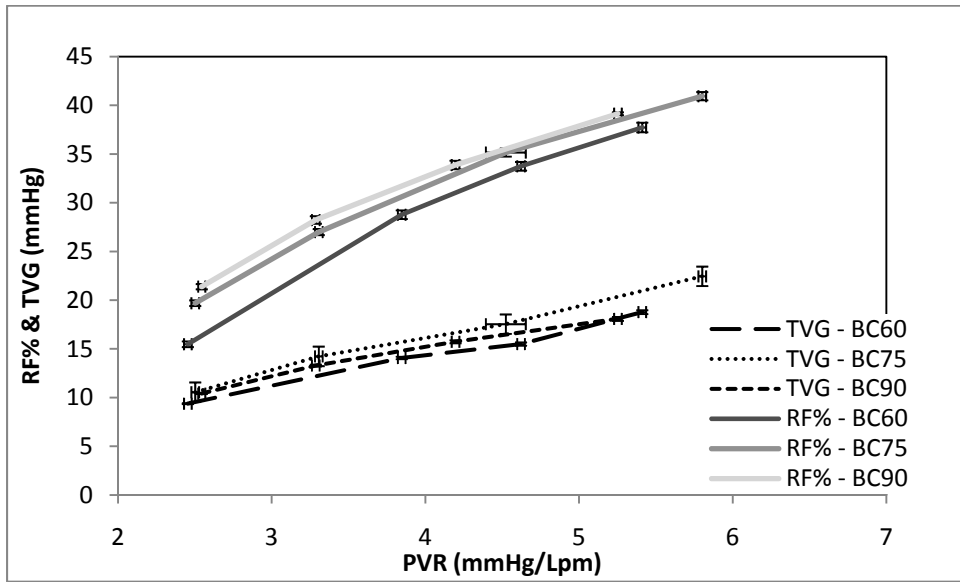
Figure 6.2: PVR vs RF% and TVG (mmHg) for all backchannel diode valves (β=0.50) with 95% confidence intervals
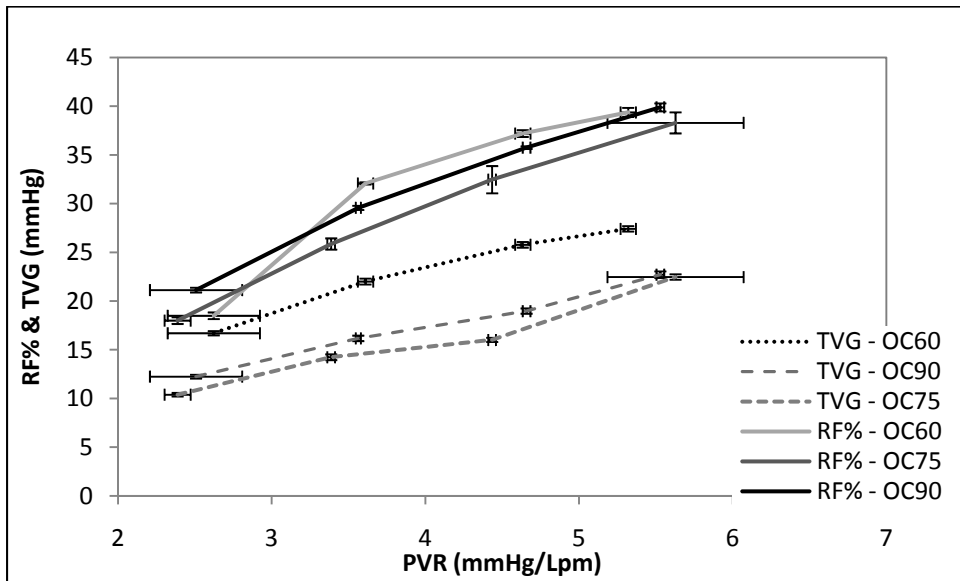
Figure 6.3: PVR vs RF% and TVG (mmHg) for all open cupsed diode valves (β=0.50) with 95% confidence intervals

Figure 6.4, Figure 6.5 and Figure 6.6 compare the effect of cusp design on the pressure gradient and RF%. Figure 6.4 shows the RF% and TVG versus PVR for the open cusped and backchannel diodes with 60˚ impingement angles. At the lowest resistance, the difference in the gradients is not significant. As the PVR increases, the open cusped diode experiences significantly higher pressure gradients than that of the backchannel diode. The open cusped diode has transvalvular gradients between 50-78% higher than that of the backchannel diodes. The behavior of the RF% for these valves again coincides with that of the TVG. The open cusped diode at pulmonary vascular resistances above 3 mmHg/Lpm has regurgitant flow up to 10% higher than the backchannel diode.

The performance of the backchannel and open cusp diode with 75˚ angles as a function of PVR is shown in Figure 6.5. There is no significant difference in the pressure gradients for either valve over the range of resistances. There is also no significant difference between the RF% values. This is contrary to the valves with $\alpha = 60˚$.

The two cusp designs when coupled with an impingement angle of 90˚ are compared in Figure 6.6. The transvalvular gradient curves are separated by a discernible difference. The open cusped diode has a slightly higher TVG than the backchannel diode. The pressure gradients are approximately 12 - 15% higher for the open cusped valve. However, the cusp design has no noticeable effect on the RF% for valves with 90˚.

In summary, for both the backchannel and open cusped diode designs, there appears to be a relationship between the valve performance and the impingement angle. The 60˚ backchannel diode has the lowest RF% and TVG for some levels of the resistance among the backchannel valves. Conversely, the 60˚ open cusped valve has markedly higher RF% and TVG measurements versus the other two valves. The valve with the 75˚ angle is the best performing open cusped design. Also, the results of this study show the effect of the impingement angle seems less influential on the backchannel diodes than on the open cusped diodes. An interaction between these factors, and possible others, is indicated.

<u>Results – Beta Ratio</u>

Three open cusped diode valves with varying orifice diameters were also tested. The pressure gradients versus PVR for all the valves are plotted in Figure 6.7. The effect of the beta ratio on the pressure gradient is great. The diode with the largest beta ratio is the same 60˚ open cusped diode tested before and has TVG values between 7 and 21.2 mmHg for PVR values between 2.6 and 6.3 mmHg/Lpm. The reduction of the orifice area results in an increase in TVG of 300-1000%. The diode with $\beta = 0.45$ has pressure gradients 39 - 57 mmHg over a range of PVR of 3 to 6 mmHg/Lpm. This range is close to the levels that are unacceptable. The diode valve with the smallest beta ratio has the highest TVG values. Over the range of resistances, the TVG does not change much. It ranges from 55.5 mmHg to 62 mmHg. The effect of the area reduction between the valve with the 0.45 and 0.40 beta ratios is less than that between the 0.45 and 0.50 beta ratios.

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The regurgitant fraction versus the pulmonary vascular resistance for the valve with different beta ratios is shown in Figure 6.8. Unlike the previous results where the valve with the lowest TVG corresponded to the valve with the lowest RF%, the valve with the smallest orifice has the lowest RF%. At the lower PVR levels, the RF% for all three valves are is around 15%. However, the rate at which the RF% changes varies based on the beta ratio. The RF% for the valve with the $\beta = 0.40$ shows little sensitivity to the pulmonary vascular resistance. The regurgitant fraction ranges from 15.6% to 20%. The increase in PVR has more effect on the middle valve as its RF% ranges from 20.6% to 34.3% for PVR values from 3.1 to 6.0 mmHg/Lpm. Finally, the diode valve with the beta ratio of 0.50 provides the least amount of resistance to retrograde flow as it has the highest RF% of the three valves. The RF% ranges from 15.4% at PVR = 2.6 mmHg/Lpm to 44% at PVR of 6.3 mmHg/Lpm.

The data shows that the beta ratio has an effect on both the pressure gradient and the regurgitant flow. This is expected as the pressure gradient across any reduction in area is correlated with the size of the opening or constant flow rates. The smaller areas also had lower RF%. At lower resistances, the difference is not as significant; however, as PVR increased the valves with the smaller openings restrict reverse flow more effectively.
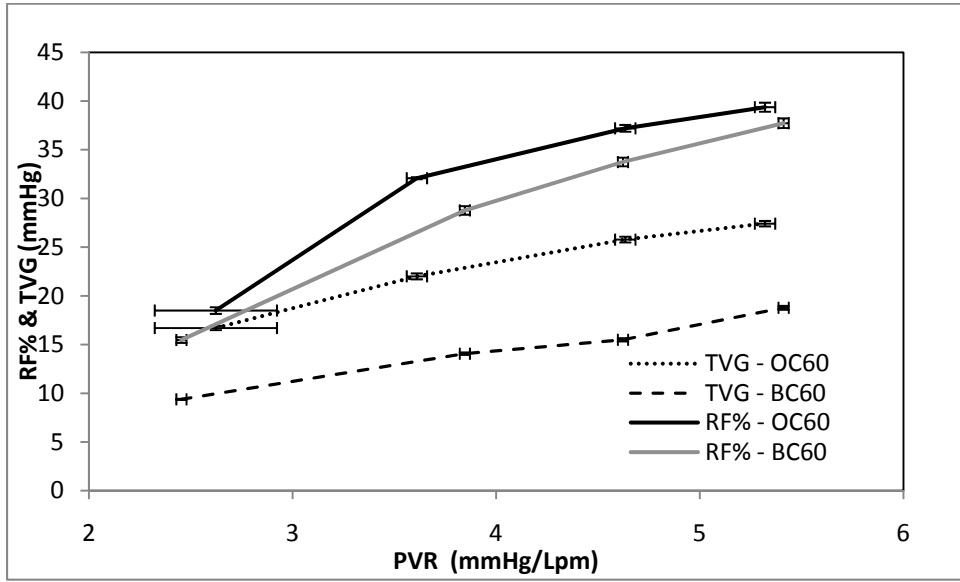
Figure 6.4: PVR vs RF% and TVG (mmHg) for diode valves with α = 60˚ (β=0.50) with 95% confidence intervals
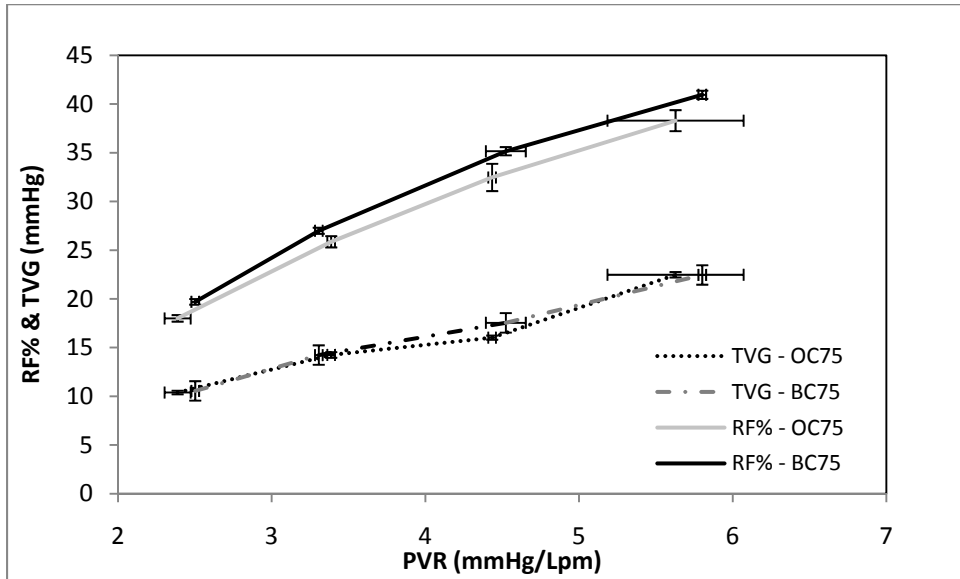
Figure 6.5: PVR vs RF% and TVG (mmHg) for diode valves with α = 75˚ (β=0.50) with 95% confidence intervals
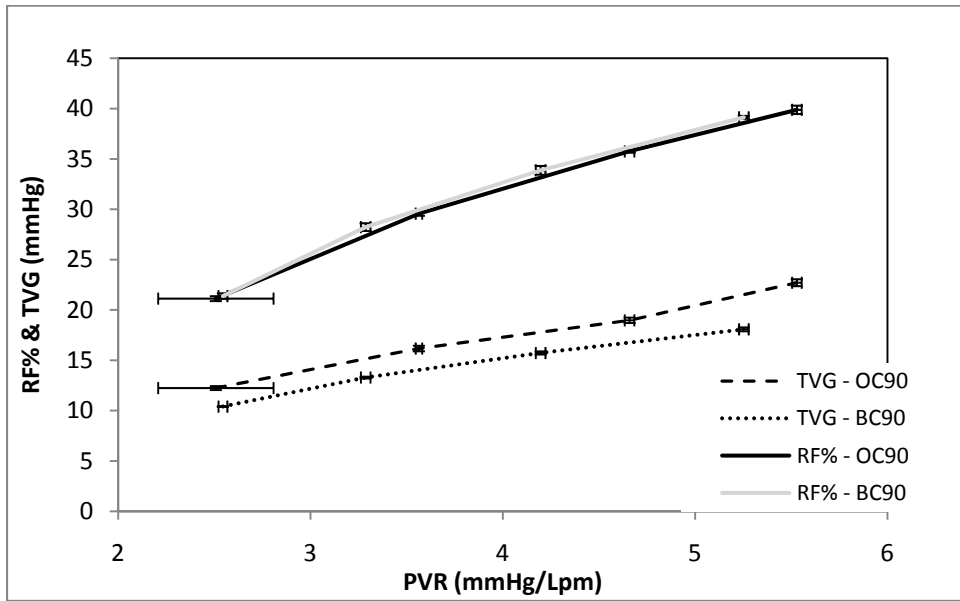
Figure 6.6: PVR vs RF% and TVG (mmHg) for diode valves with α = 90˚
(β=0.50) with 95% confidence intervals
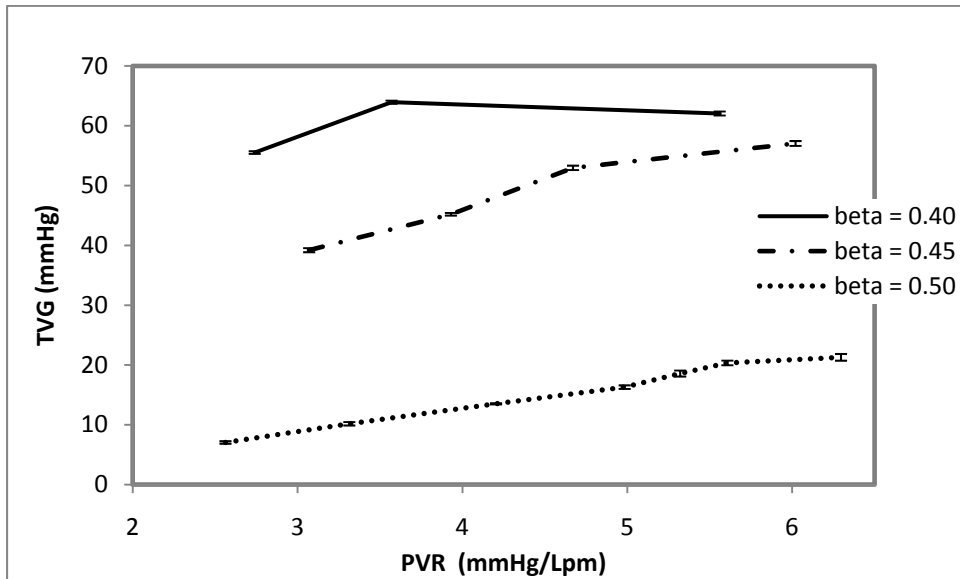
Figure 6.7: PVR vs TVG for open cusped diode valve with different beta ratios.
95% confidence interval included. Tests conducted at cardiac output of 4 Lpm.
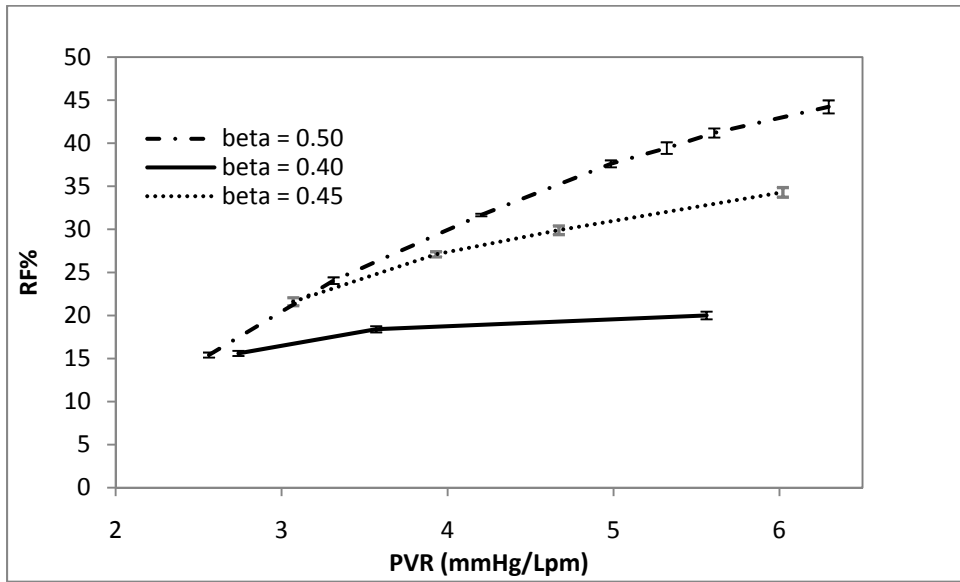
Figure 6.8: PVR vs RF% for open cusped diodes valve with different beta ratios. 95% confidence intervals included.

CHAPTER SEVEN

PARTICLE IMAGE VELOCIMETRY RESULTS

Particle image velocimetry was used to gather flow data in an open cusped diode design and a backchannel diode. The diodes were machined in stainless steel and polished. The details on each design are shown in Table 2.1 as designs 1 and 2.

Effect of Inertance

Inertance is the measure of the pressure gradient required to accelerate a fluid. It is a function of the density of the fluid, the length and cross sectional area of the tubing in which it flows. The following equation is the inertance for a tube:

$$I = \frac{\rho l}{A} \tag{19}$$

Inertance is related to the pressure gradient and the change in flow rate by equation 20.

$$\Delta p = I \frac{dQ}{dt} \tag{20}$$

It was believed that the inertance in the mock circulatory system had an effect of on the performance of the diode valve in the MPCS. This became of interest since the PIV studies were performed with a blood analog with a higher density than the performance studies. Higher inertance was believed to reduce the regurgitant fraction at a given PVR. This concept was studied using an in house algorithm developed in

Matlab®. The algorithm simulated the MPCS in lumped parameter terms. Every component of the physical system was represented in the lumped parameter model (LPM).   A schematic of the system upstream of the diode valve is shown in Figure 7.1. The resistance, compliance and inertance elements were all identified. The upstream inertance is depicted as L_{VH}. A complete explanation of the algorithm is in Appendix A.

Using this model, the inertance (L_{VH}) was varied and the resulting PVR, PVC, TVG and RF% were found. The system inertance based on using water/glycerin and the standard amount of ventricle hose used in the system was found to be 0.088 mmHg-s/mL. The simulation was run at a PVR = 3.0 mmHg/Lpm and a cardiac output of 5.3 Lpm. The resulting RF% was 11.1%. The ventricle inertance was reduced by a factor of 2, 4 and 8 and the RF% did not change. Decreasing the ventricle hose length below the standard had no effect on the RF%. This suggested that standard hose length was acceptable.

The model was also run using levels of ventricle hose inertance greater than 0.088 mmHg-s/mL. As the inertance was increased, the RF% decreased. When L_{VH} was raised by 70%, the RF% decreased to 8.6%. Since the density of the water/glycerin/NaI blood analog used in the PIV studies was 1.5 times higher than the water/glycerin solution, the inertance was also 1.5 times higher. A table with complete results from the simulation is located in Appendix A.

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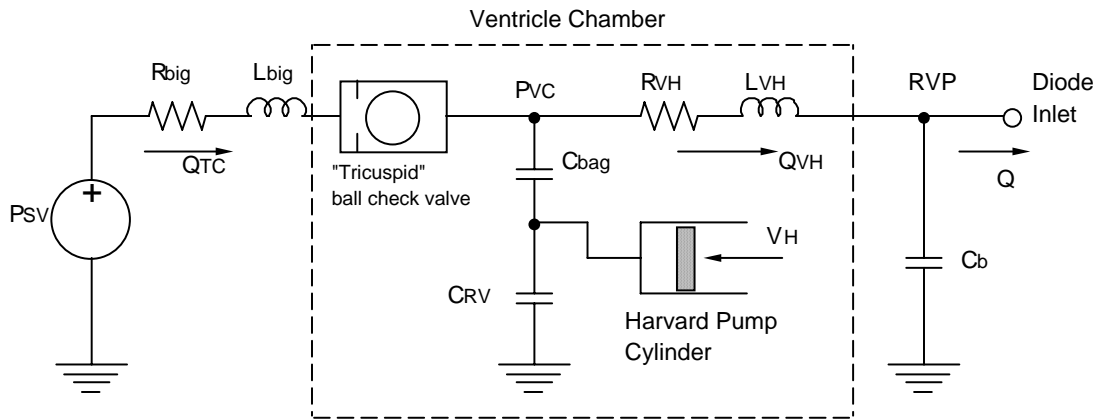
Figure 7.1. Lumped parameter model for the upstream of the Mock Circulatory System.

The results from the model support the conjecture that the RF% in a system using the NaI solution would be lower than the RF% of a system using just water/glycerin at the same resistance. Thus, the following PIV results have lower RF% for given values of PVR. For example, in the parametric study, the RF% for the backchannel diode with a 60 angle at PVR = 5.4 mmHg/Lpm was 38% (Figure 6.2). However, in this study for the same valve the RF% = 30% for a PVR of 6.85 mmHg/Lpm.

Determination of Time Delays

The accuracy of the particle image velocimetry measurements is dependent upon the time between the two illumination pulses. A delay needs to be long enough so that the displacement of the particles is determinable, but short enough to avoid particles with an out-of-plane velocity component leaving the light sheet between subsequent

illuminations [118]. In this study, the time delay, Δt in microseconds, varied for each time step of the cardiac cycle and for each PVR tuning. The flow rate of each PVR settings was recorded. The magnitude was checked in 50 ms intervals beginning with the start of systole. This flow rate was converted from liters/minute to an equivalent average velocity. The pixel calibration was used to determine a Δt that corresponded with a particle movement of roughly 10 pixels. The time delay accuracy was checked by comparing the flow rate measured experimentally with the electromagnetic flow probe with the calculated flow rate using the PIV results. At a particular time step, the average velocity was found by performing a numerical integration on lines of constant x values.

<p style="text-align:center;">Discussion of Data Sets</p>

The plane of view for the particle image velocimetry was an overhead view that captured the artery section just downstream of the valve as well as the pulmonary artery branch. The central plane was grabbed without issue and the full area as shown in Figure 7.2. The laser sheet for the offset planes did not light the pulmonary branch sufficiently. Most likely this was a result of the minor mismatch in the refractive indices. Therefore, the full view of the pulmonary artery branch will be presented for the central plane; however, only data from the main pulmonary artery will be presented for the offset planes.

The PIV results for the two diode types are present here. The diodes were tested at four different PVR levels of ~3 mmHg/Lpm, ~4 mmHg/Lpm, ~5 mmHg/Lpm and ~6 mmHg/Lpm and will be referred to as Cases 1 - 4. For each case, four of the 16 time

steps within the cardiac cycle will be discussed. The times represent distinct period within the cycle early systole (t = 150 ms), peak systole (t = 350 ms), mid diastole (t= 550 ms), and late diastole (t = 750 ms). The flow patterns at each interval will be described. The level of high velocities, viscous shear stresses and Reynolds shear stresses (RSS) will be identified for every case. The data in the offset plane of view for the same times will also be reviewed. Select cases will be presented in the main text. The remaining cases are included in Appendix B.
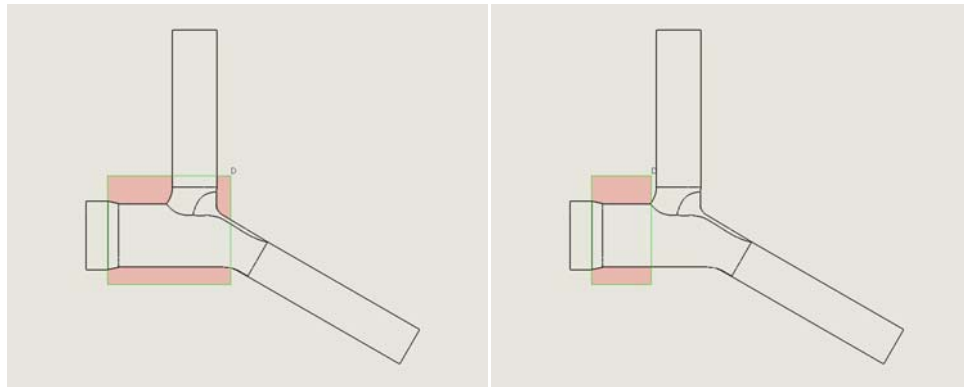
Figure 7.2 Coverage area for the (a) Central PIV plane and (b) offset PIV planes

Baseline PIV Data

The pulsing operation of the mock circulatory system generates a measurable amount of cyclical vibration. The system sits on an optics table that does dampen this

vibration; however, some residual vibration may exist. Since any movement in the camera or the test section can affect the time values of the PIV measurements, a method to determine the amount of this 'noise' was established.

The 'noise' resulting from any uncertainty in the PIV measurement was ascertained by measuring a zero flow case to determine the effects of the system operation on the measurements themselves. To do this, valves immediately upstream and downstream of the test section were closed. However, the system otherwise operated normally. The pulse rate of 75 bpm was applied to the ventricle by the mechanical pump and fluid was circulated to the head tanks via the circulation pump. Measurements were acquired normally and analyzed. Peak Reynolds shear stresses of up 2 dynes/cm^2 were created by the system effects. Peak viscous shear stresses of up to 1.45 dynes/cm^2 were observed in the same case. Yet, the average values were significantly lower. The mean turbulent and viscous shear stresses were on the order of 0.1 dynes/cm^2 and 0.07 dynes/cm^2, respectively. These values are taken as the upper limits of noise due to vibration on the acquired data.

Open Cusped Diode Results

Tests were run on the 25 mm open cusp diode. The system was adjusted to 75 bpm with an average flow rate of 5 Lpm. The pulmonary vascular resistance (PVR) of the MCPS was regulated and set to achieve varying levels of RF%. The results for three PVR values will be presented. They are: Case 1 - PVR = 3.1 mmHg/Lpm, Case 3- PVR = 5.1 mmHg/Lpm, and Case 4 - PVR = 6.1 mmHg/Lpm. The central plane PIV results will

be discussed for all three cases. Only the Case 1 offset plane results will be discussed in detail here. The remaining results discussion is in Appendix B.

Case 1

The pressure and flow curve for the low case of PVR = 3.1 mmHg/Lpm is shown in Figure 7.3. The regurgitant fraction for this circumstance is 1.84%. The PIV results show that flow patterns throughout the cardiac cycle. First, the results from the central plane are presented.

Early systole (t = 150 ms)

During early systole, uniform antegrade flow exists the main arterial section Flow is seen in the arterial branches as well. It is relatively undisturbed in the left pulmonary artery (LPA) in comparison to the right. . The velocities in the main pulmonary artery (MPA) range between $0 - 0.15$ m/s with an average of 0.08 m/s.

Figure 7.4 also shows the hydraulic shear stresses for this case. The uniform flow profile results in the highest stresses being near the walls. The magnitudes of these stresses are under 5 dynes/cm^2. However, statistical analysis shows that these values are significantly different than those measured in the baseline case suggesting that the values are valid.

At 150 ms after the start of systole there is little disturbance in the flow. The peak shear stresses are at the RPA branch where MPA axial flow is moving around the 90° arterial bend and in the middle of the bifurcation where the primary and secondary flows

meet (Figure 7.4). The RSS are low in comparison to the rest of the cardiac cycle and this is shown in Figure 7.5.

Peak systole (t = 350 ms)

The jet develops and moves downstream through the MPA reaching the RPA and LPA branches by 200 ms after the start of systole. It continues to accelerate downstream for another 150 ms. The highest flow rate, considered to be peak systole, occurs between 350 and 400 ms after the start of systole. Figure 7.6 shows the flow and shear stress fields at 350 ms. The entrained region is defined by moving vortical cells traveling along the MPA wall leaving behind region of recirculation from $r = \pm 7$ mm to ± 11.5 mm as shown in Figure 7.6. As the jet entrainment vortex forms around the central core a region of recirculation is seen to form as the flow diverges into the right pulmonary artery (RPA). The jet impinges on the artery wall at the bifurcation. The maximum velocity at this point in the cardiac cycle is 1.28 m/s and the average velocity is 0.410 m/s. In the RPA, the velocities are highest along the outer wall (more downstream) and weaken toward the inner wall. Along the outer wall, the velocities are on the order of 0.400 m/s.

The peak viscous shear stresses for this case are approximately 30 dynes/cm^2 (Figure 7.6). The wall shear stresses along the outer RPA wall are around 15 dynes/cm^2, which is relatively high in comparison to the rest of the field.
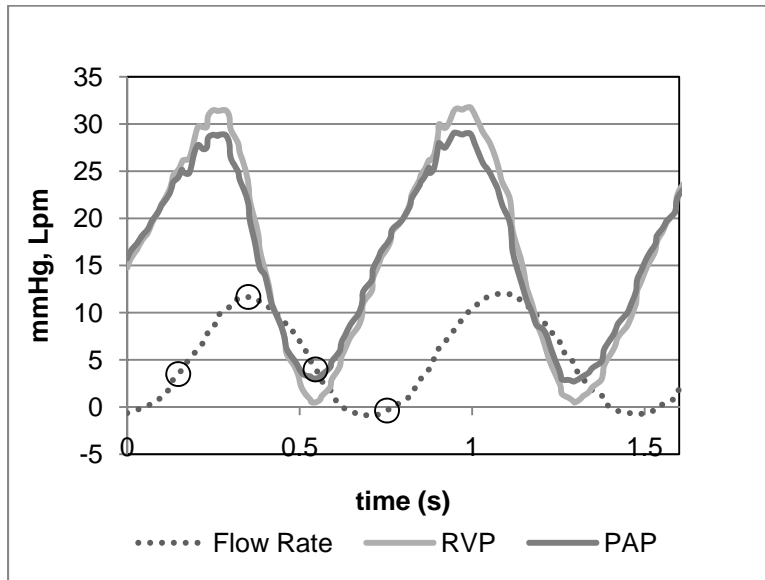
Figure 7.3. Flow and Pressure curve for PVR = 3.1mmHg/Lpm
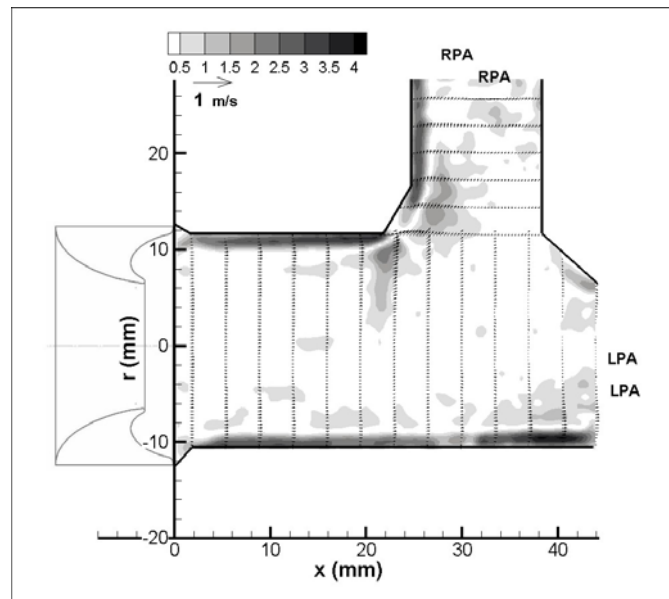
Figure 7.4. Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after the start of systole for PVR = 3.1 Lpm
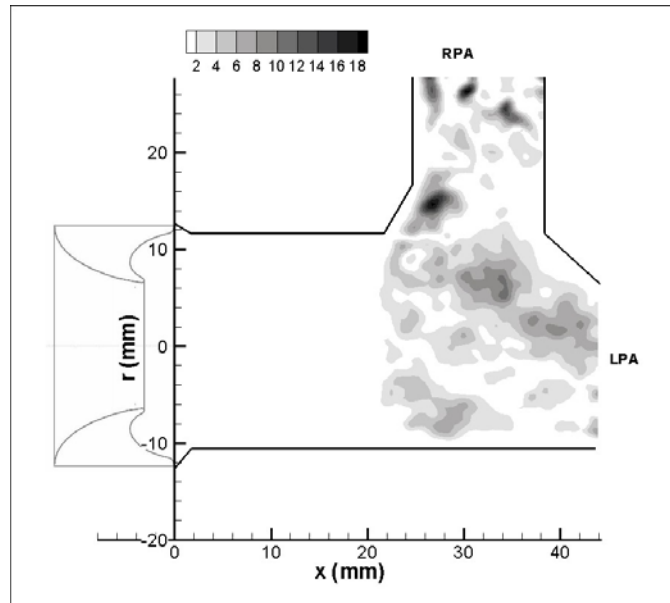
Figure 7.5: Reynolds shear stress field (dynes/cm^2) for the open cusped diode
at 150 ms after the start of systole for PVR = 3.1 mmHg/Lpm, central plane

The action of an effective momentum diode creates areas of impinging momentum resulting in mixing. Such mechanisms are prone to large scale flow disturbances. The highest RSS values are about 600 dynes/cm^2 during peak systole (t = 350 ms) in Figure 7.7. The highest levels of RSS are seen 25 mm downstream in the area of the arterial bifurcation in the upper radial location near the RPA. It is here that the turbulence is created by the recirculating flow rejoining the flow in the main pulmonary artery per Figure 7.6. In the lower radial location, the peak Reynolds shear stresses are measured at approximately 400 dynes/cm^2 with surrounding areas having measured stress levels of greater than 300 dynes/cm^2. This is in the area of recirculation entering the LPA.

Mid Diastole (t = 550 ms)

Figure 7.8 shows the flow and viscous shear stresses near the peak mid diastole phase (t = 550 ms). The jet structure can still be discerned with peak velocities not less than about 0.6 m/s, and with an average velocity of 0.186 m/s. At the outer RPA, the velocities are still slightly above 0.400 m/s. The region of recirculating flow is still present as flow momentum has carried it into the right and left pulmonary arteries.

The bulk shear stresses are still the highest along the edges of the central jet shown in Figure 7.8. The values are about 15 dynes/cm^2, half that observed at peak systole (just as the velocities were). The wall shear stresses in the RPA, however, are unchanged at approximately 15 dynes/cm^2 since the velocities also remained the same during this time interval.

Figure 7.9 shows the RSS field and the peak RSS measurements take place where the flow diverges into the RPA and LPA. Moreover, in the area in which the secondary RPA flow wraps around and meets the MPA flow, the Reynolds shear stresses have lessened to around 200 dynes/cm^2. The area of recirculating flow leading into the LPA, however, remains disturbed and has turbulent shear stress values of 200-300 dynes/cm^2.

Figure 7.6: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.7: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 350 ms after the start of systole for PVR = 3.1 mmHg/Lpm, central plane

Finally, Figure 7.10 shows the flow region during mid-diastole at 750 ms after the start of systole. By this point in the cycle the retrograde flow is established throughout the test section. The velocity profile is uniform as the branch flow converges in the main PA; the average flow is about -0.072 m/s across the test section. This corresponds with the negative flow rate measured between 620 – 800 ms (Figure 7.3). The retrograde motion is well behaved and allows the flow to wash artery walls and eliminate regions of recirculation. Only at the region of the bifurcation is stasis flow measured. The wall stresses are less than 5 dynes/cm^2. This is consistent with the uniform flow.

Figure 7.11 shows the field of turbulent shear stresses. The peak stresses are less than 50 dynes/cm^2. These measured stresses are well above the noise measured in the zero flow case thus suggesting that the 50 dynes/cm^2 is reflective of the turbulent shear stresses in the flow.

Figure 7.8. Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.9: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 550 ms after the start of systole for PVR = 3.1 mmHg/Lpm, central plane

Figure 7.10. Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.11: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 750 ms after the start of systole for PVR = 3.1 mmHg/Lpm, central plane

Case 1 - Offset planes

The offset flow plane was 5 mm from the central plane. Therefore, the radius of the cross section in this view is 10.75 mm versus the 11.85 mm measured in the central plane. The offset flow plane has similar characteristics as the central plane. Also, in the offset plane of view, the laser sheet did not adequately light the arterial branches. Therefore, the field of view is only the main artery.

Early systole (t = 150 ms)

At 150 ms after the start of the cycle (Figure 7.12) the velocities are on the order of -0.0440 m/s with maximum values of 0.102 m/s. As time progresses, the jet flow emerges from the diode valve. The width of the jet is expectedly narrower than that along the central plane of pulmonary artery. Vortical structures are present, and begin approximately 6.5 mm away from the axial centerline in both radial directions.

The viscous stresses in the offset planes were analyzed for comparison to the central plane data (Figure 7.12). The data from both planes are similar in trend and magnitude. The wall shear stresses are approximately 3.7 dynes/cm^2. This is of similar magnitude as the wall shear stresses seen in the central plane (Figure 7.4).

As with the viscous shear stresses, there is little difference between the Reynolds shear stress fields in the offset and central planes. However, since the more notable turbulent shear stresses in the central plane fields occur more than 20 mm downstream the offset plane data is abbreviated and does not have as much detail. In Figure 7.13,

RSS map for the early systole case is shown. The peak turbulent stresses within the first 22 mm of the diode are on the order of 5 dynes/cm^2.

Peak systole (t = 350 ms)

These areas are well defined during peak systole, 350 ms after the start of the cycle, as seen in Figure 7.14. The average and peak velocities at this phase were found to be 0.308 m/s and 1.17 m/s, respectively. The peak shear stresses occur along the edge of the jet structure with values of 28 dynes/cm^2. At 350 ms after the start of systole, the magnitudes are on the same level observed in the central plane (within 22 mm of the valve exit). As seen in Figure 7.15, the peak turbulent stresses are 330 dynes/cm^2.

Mid Diastole (t = 550 ms)

Figure 7.16 shows the flow at mid diastole. The velocity is still dependent on the radial location. The maximum velocity is 0.545 m/s which is about half of what was seen at peak systole. The average velocity is 0.129 m/s. The peak stresses are along the edges of the centrally formed jet. The peak values are 10 dynes/cm^2. Likewise, at 550 ms into the cycle the RSS fields are similar for the offset and central planes. The stresses reach up to 143 dynes/cm^2. This can be seen by comparing Figure 7.9 and Figure 7.17.

Late Diastole (t = 750 ms)

During diastole the velocities are on the order of -0.075 m/s and are relatively uniform (Figure 7.18). The axial velocity peaks at -0.152 m/s. The wall shear stresses are just below 4 dynes/cm^2 during diastole, 750 ms after the start of the cycle. All of these

offset measurements are similar to the central plane measurements. The offset plane RSS measurements are shown in Figure 7.19. There is little disturbance; the turbulent shear stresses are in the range of 22 dynes/cm^2.

Case 3

The pressure and flow curves for the open cusped diode at this setting are shown in Figure 7.20. The flow rates vary from -4.5 Lpm to 16 Lpm. The four 150 ms time intervals are marked off with circles. At 350 ms into the cycle, the peak flow rate has not been reached. Peak systole takes places at 450 ms and is also denoted on the flow curve. Therefore, for this instance, five points will be presented. The pulmonary vascular resistance is 5.1 mmHg/Lpm and the RF% is 18%.

Figure 7.12. Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.13: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 150 ms after the start of systole for PVR = 3.1 mmHg/Lpm, offset plane

Figure 7.14. Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.15:Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 350 ms after the start of systole for PVR = 3.1 mmHg/Lpm, offset plane

Figure 7.16. Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR = 3.1 Lpm

Figure 7.17: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 550 ms after the start of systole for PVR = 3.1 mmHg/Lpm, offset plane
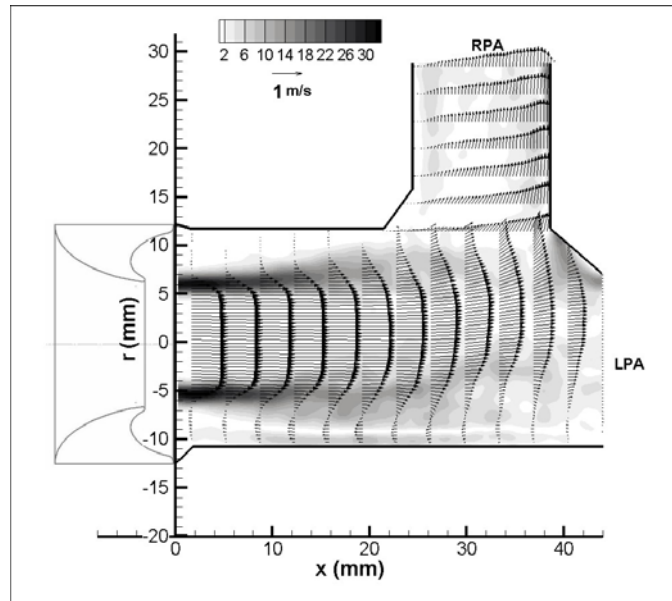

Figure 7.18. Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cushed diode at 750 ms after the start of systole for PVR = 3.1 Lpm
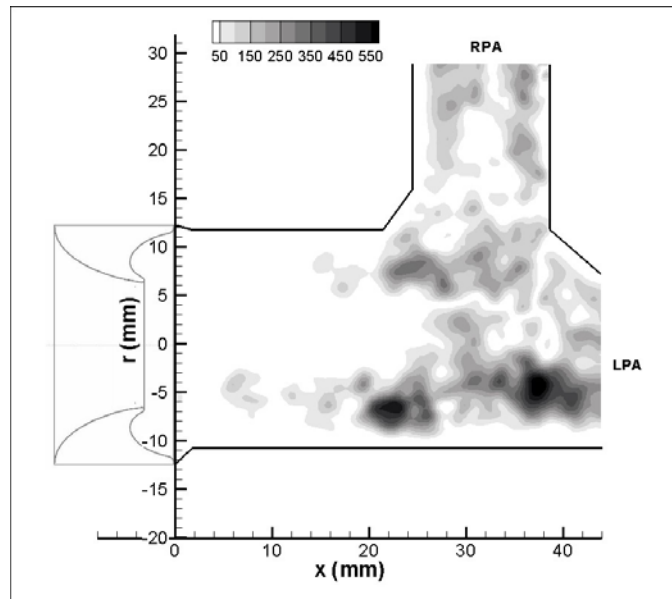
Figure 7.19: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 750 ms after the start of systole for PVR = 3.1 mmHg/Lpm, offset plane
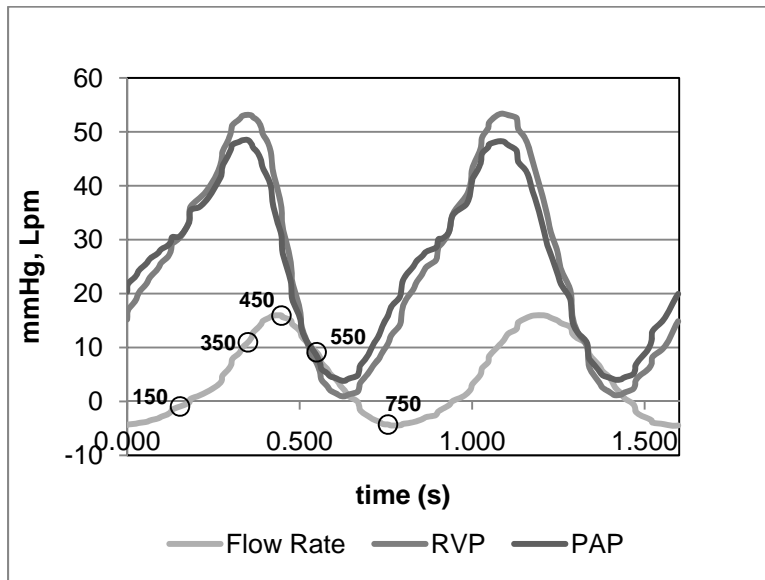
Figure 7.20: Flow and pressure curves for the open cusped diode, PVR = 5.1 mmHg/Lpm

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Early Systole (t = 150 ms)

Figure 7.21 is the flow profile at 150 ms for the PVR = 5.1 mmHg/Lpm case with axial and radial vector spacing, respectively. Unlike the Cases 1 and 2, the flow at this point is still transitioning from retrograde to antegrade. Uniform reverse flow exists in the right and left pulmonary arteries. The two flows combine and form reverse axial flow in the main artery. The peak reverse velocity is about 0.186 m/s and the average velocity in the main pulmonary artery is -0.208 m/s.

The bulk flow shear stresses are overall very low at 150 ms after the beginning of systole. The peak stresses within the field reach 2-3 dynes/cm^2 along the regions of recirculation (Figure 7.21). The peak wall shear stresses are in the RPA at 4 - 5 dynes/cm^2 resulting from the reverse flow.

The turbulence shear stresses for the field at 150 ms after the start of systole are shown in Figure 7.22. The peak RSS values are 130 dynes/cm^2. This is higher than they were in the PVR = 4.3 case at 150 ms (50 dynes/cm^2). Figure 7.21 shows jet flow emerging from the RPA into the path of the LPA retrograde flow. The RPA flow has more momentum than at lower PVR values; thus, there is more mixing and more turbulence. The region of peak turbulent shear stresses is isolated at 32 mm downstream and about 3.5 above the centerline. There is no measureable RSS in the regions of stasis flow.
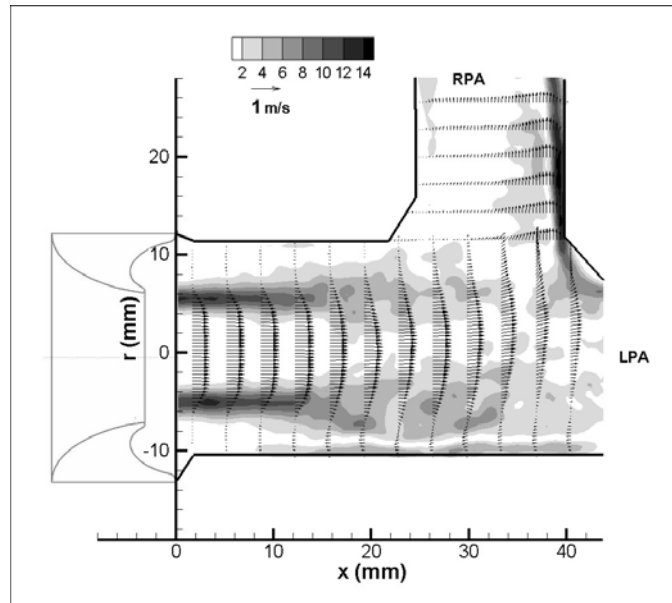
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Figure 7.21: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after the start of systole for PVR = 5.1 mmHg/Lpm
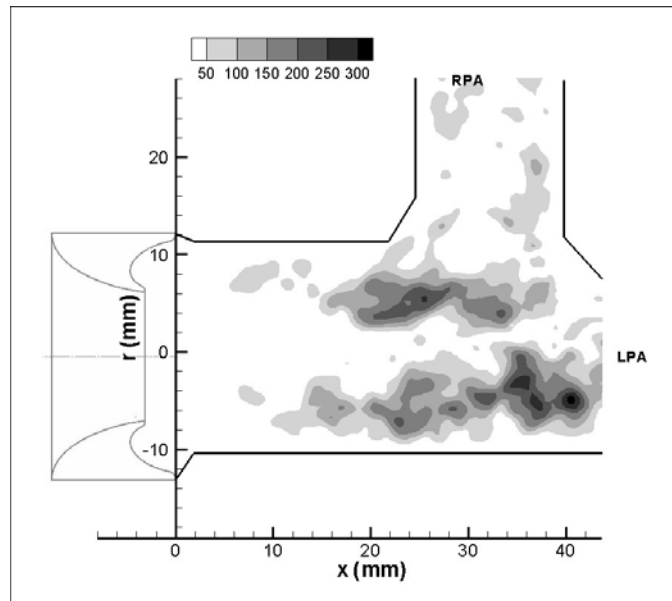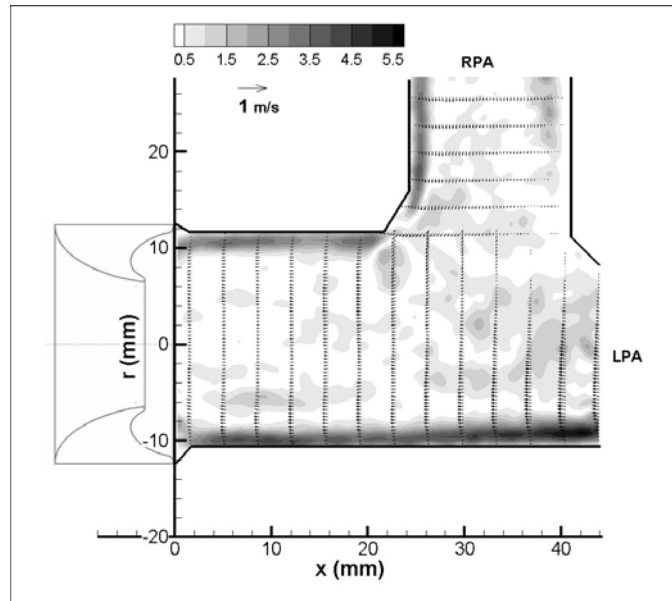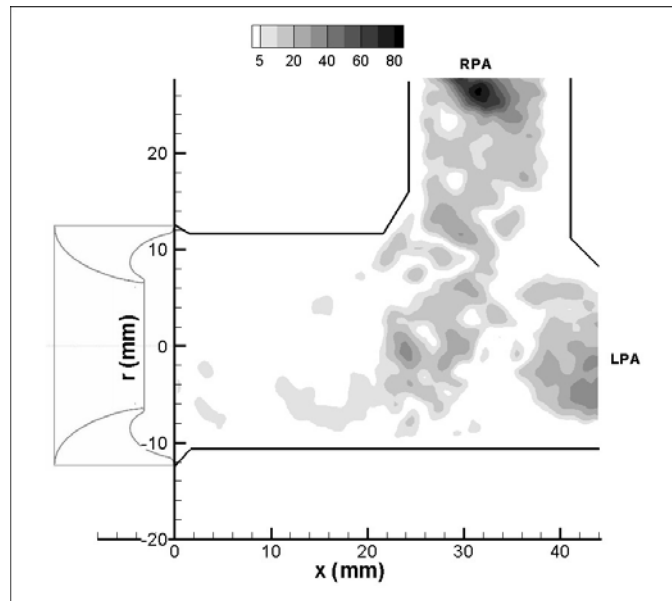

Figure 7.22: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 150 ms after the start of systole for PVR = 5.1 mmHg/Lpm, central plane

Mid systole (t = 350 ms)

During mid systole, a central jet is observed to exit the valve, travel into the LPA and impinge on the wall of the LPA as seen in Figure 7.23. There are rolling vortices in the main artery, the larger of the two at the lower MPA wall. The flow in the right artery has strong axial component along the distal wall. This is more like the flows at the low PVR = 3.1 mmHg/Lpm case as opposed to the PVR = 4.3 mmHg/Lpm case where the primary flow makes a relatively smooth turn into the RPA. In the left pulmonary artery the jet structure flows mostly unimpeded. The area of recirculation ends at the LPA entrance, near 32 mm downstream. The maximum velocity magnitudes are 1.63 m/s. The average axial velocity in the MPA is 0.576 m/s.

The highest bulk flow shear stresses are along the edges of the jet (Figure 7.23). This is similar to what occurs during peak systole at lower PVR values. The peak stresses measure approximately 45 dynes/cm^2. The wall shear stresses along the distal RPA wall are just over 16 dynes/cm^2. Also, the viscous stresses along lower LPA wall where the flow reattaches are about 14 dynes/cm^2.

The Reynolds shear stress field for the PVR = 5.1 mmHg/Lpm during mid systole is shown in Figure 7.24. The values range from 0 to 700 dynes/cm^2. The peak at 700 dynes/cm^2 is at the bend between the right and main arteries where flow separation takes place. The Reynolds shear stresses measures ~300 dynes/cm^2 in the area of recirculation in the RPA and entering the LPA.

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Figure 7.23: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR = 5.1 mmHg/Lpm

Figure 7.24: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 350 ms after the start of systole for PVR = 5.1 mmHg/Lpm, central plane

Peak Systole (t = 450 ms)

The peak flow rate occurs 450 ms after the start of systole. The flow and viscous shear stress fields are shown in Figure 7.25. The entrained jet structure is well developed. It travels into the LPA and impinges on the wall of that artery branch. The average velocity in the main pulmonary artery is 0.583 m/s. the velocity peaks at 1.65 m/s. The flow profile in the RPA is skewed to the distal wall where velocities measure up to 1.0 m/s.

The highest bulk flow shear stresses are along the edges of the jet (Figure 7.25). The peak stresses again measure approximately 45 dynes/cm^2. The wall shear stresses at the site of impingement where the flow diverges are approximately 22 dynes/cm^2. The viscous stresses along the distal RPA wall and the lower LPA wall where the flow reattaches are about 10 dynes/cm^2.

Figure 7.26 is the Reynolds shear stresses field at peak systole. The measurements peak at 1100 dynes/cm^2. The peak Reynolds shear stress is approximately 650 dynes/cm^2 in the area that the recirculating flow rejoins the primary flow in the MPA. This region of disturbance has travelled downstream to about 30 mm from the valve exit. Another area of high RSS is in the lower radial location near the MPA and LPA branch where they reach their highest value of 1100 dynes/cm^2 at this point.
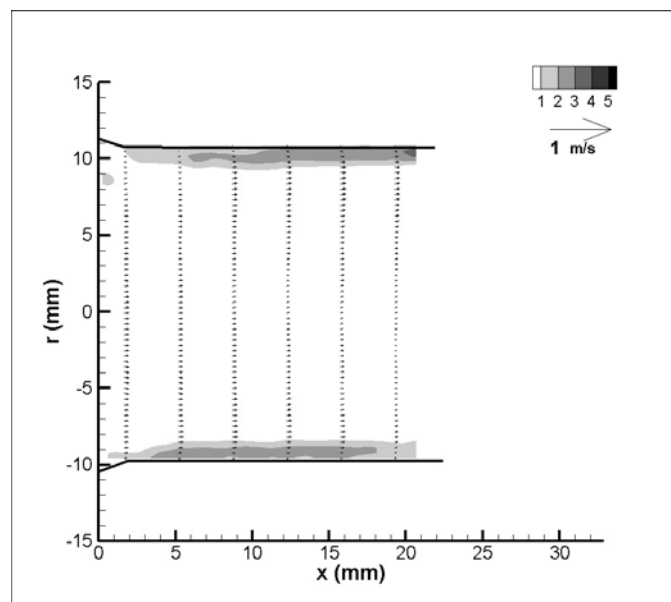
Figure 7.25: Central plane flow and viscous shear stress
(dynes/cm^2) field for the open cusped diode at 450 ms after the
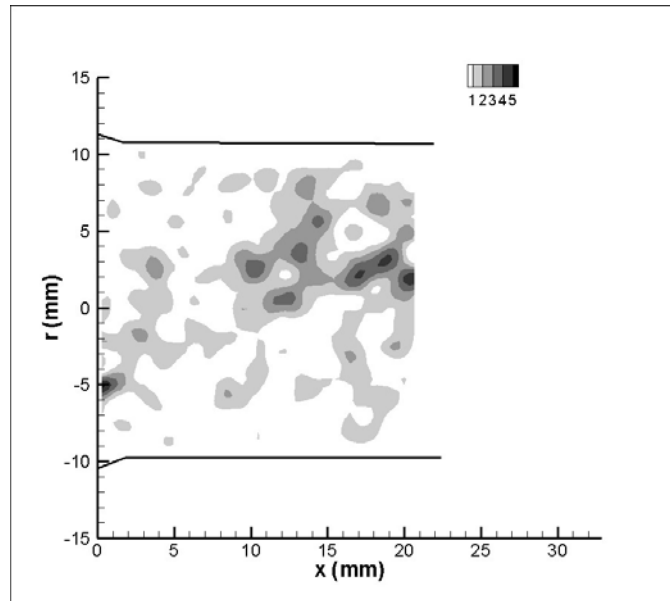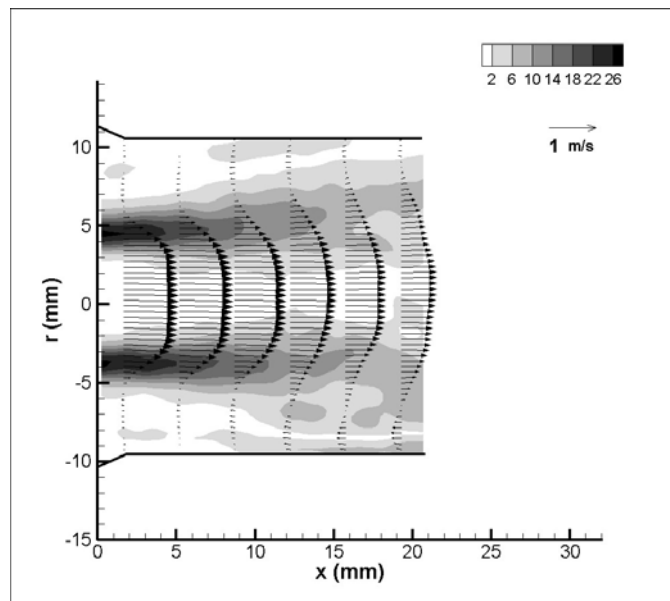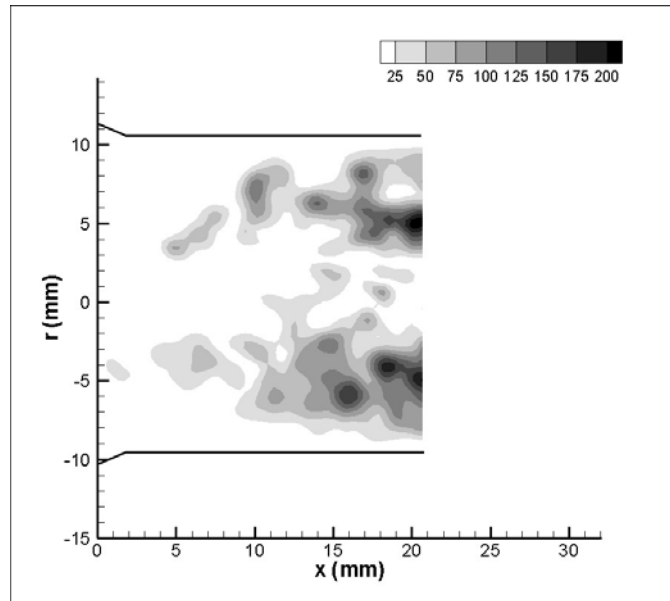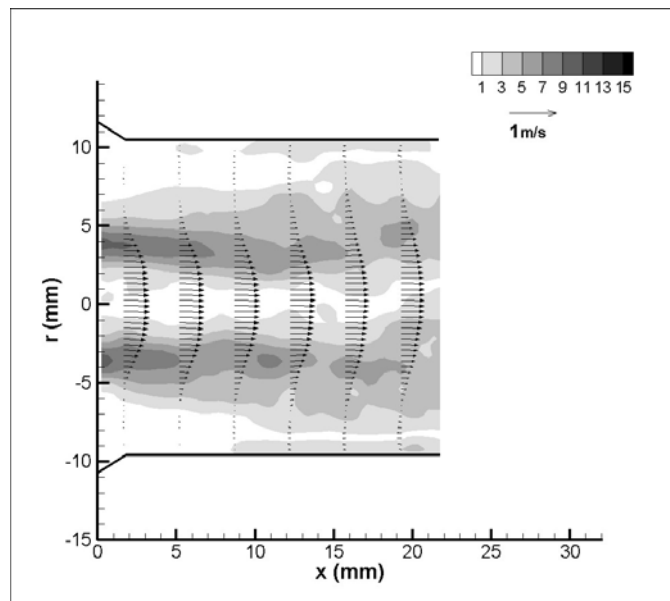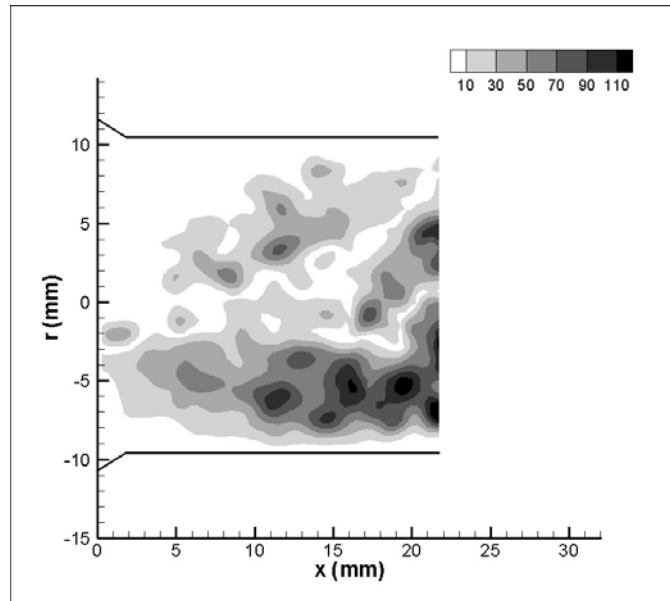start of systole (peak) for PVR = 5.1 mmHg/Lpm

Figure 7.26: Reynolds shear stress (dynes/cm^2) field for the open cusped
diode at 450 ms after the start of systole (peak) for PVR = 5.1 mmHg/Lpm

Mid Diastole (t= 550 ms)

Figure 7.27 shows the flow and bulk shear stress profiles at mid diastole. The secondary flow from the right pulmonary artery is recirculating into the main branch. The region of flow separation along the lower MPA and LPA walls has lengthened. The highest velocities are about 0.881 m/s, one half of the velocities measured during peak systole. The average velocity in the main artery is about half of the peak systole average velocity at 0.282 m/s.

As with the earlier described cases, at 550 ms after the start of the cycle, the bulk shear stresses are still the highest along the edges of the central jet with values up to 23 dynes/cm^2 as seen in Figure 7.27. The shear layer has extended as the area of flow separation lengthened. Moreover, the wall shear stresses in the RPA are between 14 – 20 dynes/cm^2.

In Figure 7.28, the RSS field for 550 ms after the start of systole is shown. The turbulent stresses reach as high as 700 dynes/cm^2 during mid diastole. It is higher where flow develops near the LPA entry (Figure B.6). The stresses are approximately 300 dynes/cm^2 where the RPA recirculating flow and the MPA flow converge.

Late Diastole (t = 750 ms)

At the 750 ms after the systolic start, there is prevalent retrograde flow in the entire pulmonary artery (Figure 7.29). The peak velocities are about -0.500 m/s and

averaged at -0.196 m/s in MPA. The flow field is relatively uniform as the flow is well organized and there is little mixing.

At 750 ms into the cardiac cycle, the shear stresses are around 7 dynes/cm^2 along the walls of the RPA and the lower MPA and LPA (Figure 7.29). There is another area of relatively high shear stress near the branch between the main and right pulmonary arteries.

Figure 7.30 show the Reynolds shear stresses for the PVR = 5.1 mmHg/Lpm case at t = 750 ms. The magnitudes are higher at this condition than in the lower PVR cases. The peak stresses are around 120 dynes/cm^2 where the flow converges at the left and right pulmonary artery branch. Mixing also occurs between the 3 arteries and generates turbulent shear stresses of about 120 dynes/cm^2.

Case 4

The final condition under which the open cusped diode was tested was at a PVR = 6.12 mmHg/Lpm and a RF% = 29.9%. The pressure and flow curves are shown in Figure 7.31.

Figure 7.27: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR = 5.1 mmHg/Lpm

Figure 7.28: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 550 ms after the start of systole for PVR = 5.1 mmHg/Lpm, central plane
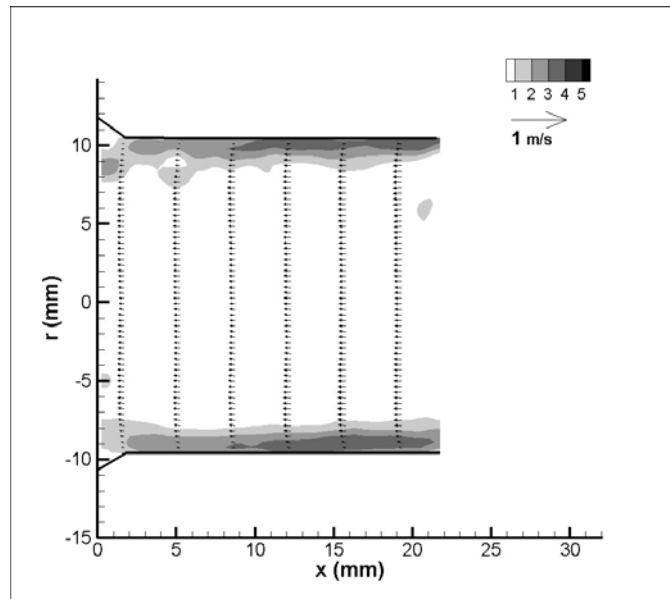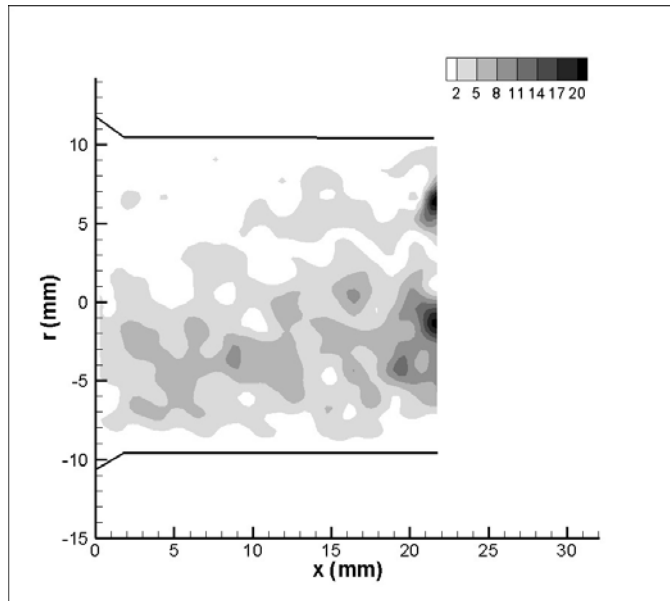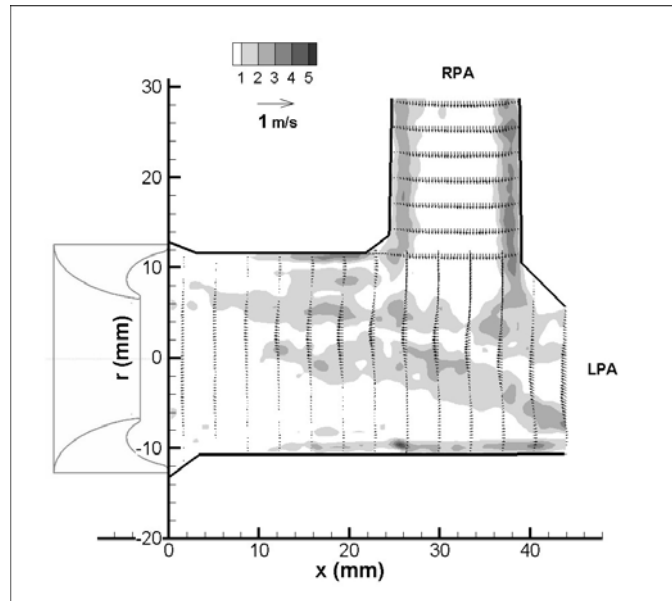
Figure 7.29: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR = 5.1 mmHg/Lpm
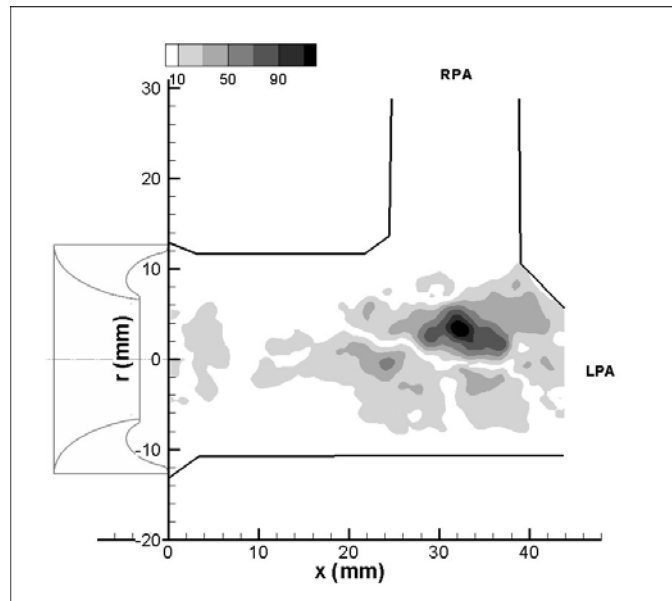

Figure 7.30: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 750 ms after the start of systole for PVR = 5.1 mmHg/Lpm, central plane

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Figure 7.31: Pressure and flow curve for the open cusped diode at
PVR = 6.1 mmHg/Lpm

Early Systole (t = 150 ms)

Figure 7.32 shows the flow and viscous shear stress field at 150 ms after the start
of systole. The flow is uniform in the main pulmonary artery. However, there is a small
region of retrograde flow at the lower MPA wall. The average axial velocity in the MPA
is 0.115 m/s and the peak velocity is 0.289 m/s. The flow into the artery branches is also
fairly uniform.

The highest occurring shear stress is at the walls of the MPA (Figure 7.32). The
peak shear stress is 8.6 dynes/cm^2. Another shear layer exists just above the lower MPA
wall between the retrograde and antegrade flow.

The turbulent shear stress field is plotted in Figure 7.33. The levels of turbulent shear stress reach 65 dynes/cm^2. One elevated region is near where flow from the main artery turns in the right branch.

Peak Systole (t = 350 ms)

At the point of maximum flow rate, there is again a strong central jet present in the flow field (Figure 7.34). There are areas of recirculation in both the upper and lower part of the MPA. The jet flow strikes the artery wall at the bifurcation and extends well into the left pulmonary artery. The flow in the RPA is skewed strongly toward the distal wall as momentum carries the flow downstream. In the MPA, the average and maximum flow speeds are 0.860 m/s and 2.37 m/s, respectively.

The highest bulk flow stresses are located along the jet edges (Figure 7.34). The peak stresses are up to 55 dynes/cm^2. The shear layer dissipates the central core flow reaches the branch. The wall shear stresses at the distal RPA wall are as high as 10 dynes/cm^2.

The Reynolds shear stresses for peak systole are shown in Figure 7.35. One of the regions where high levels of disturbance take place is positioned in between the MPA and RPA. This is where the primary flow begins to diverge and the peak values are as high as 900 dynes/cm^2. The point where the highest overall turbulent shear stress is located is in the lower MPA and LPA in the area of recirculation. Here the RSS were measured to be 1520 dynes/cm^2.

Mid Diastole (t = 550 ms)

As the cycle progresses to 550 ms after the start of the cycle, the strength of the central core jet has lessened (Figure 7.36). There are areas of recirculation in the upper and lower MPA, in the LPA and in the RPA. The average velocity has decreased to 0.124 m/s and the maximum velocities are 0.487 m/s, nearly half of what they were at peak systole.

Figure 7.36 also shows the hydraulic shear stresses in at this point in the cardiac cycle. The flow gradient at the edges of the jet produces relatively high shear stresses. Also, shear layers are present between the retrograde flow and the walls. The maximum hydraulic shear stresses at this point are just under 9 dynes/cm^2.

The highest Reynolds shear stresses are on the order of 340 dynes/cm^2. Similar to the RSS field at peak systole, there is a region of elevated stresses at the point when the primary flow from the MPA is turning into the RPA. There is another area of mixing about 35 mm downstream of the valve exit 4 mm below the center of the artery.
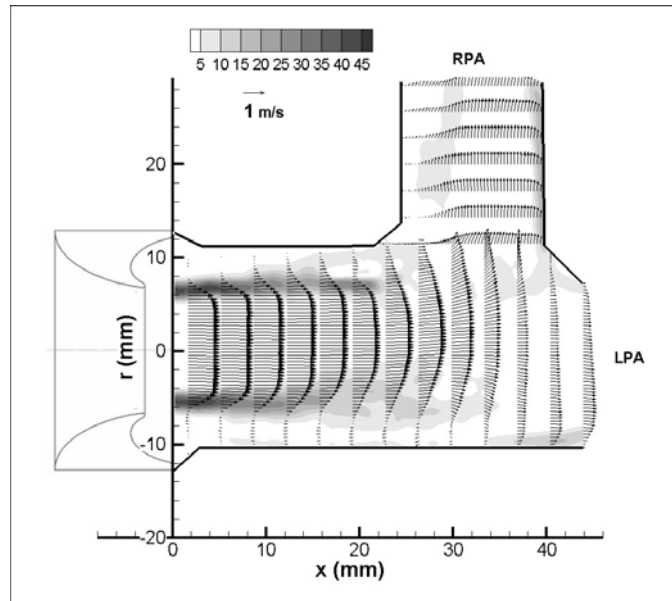
Figure 7.32: Central plane flow and viscous shear stress (dynes/cm^2) field for the
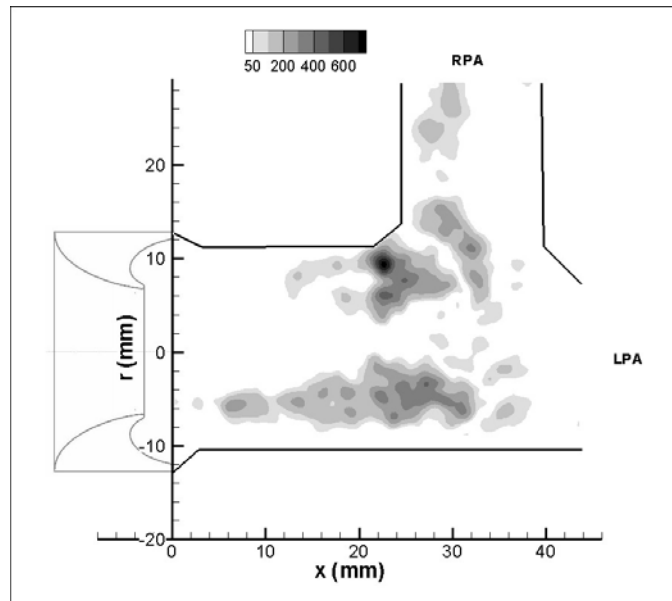open cusped diode at 150 ms after the start of systole for PVR 6.1 mmHg/Lpm

Figure 7.33: Reynolds shear stress (dynes/cm^2) field for the open cusped diode
at 150 ms after the start of systole for PVR = 6.1 mmHg/Lpm

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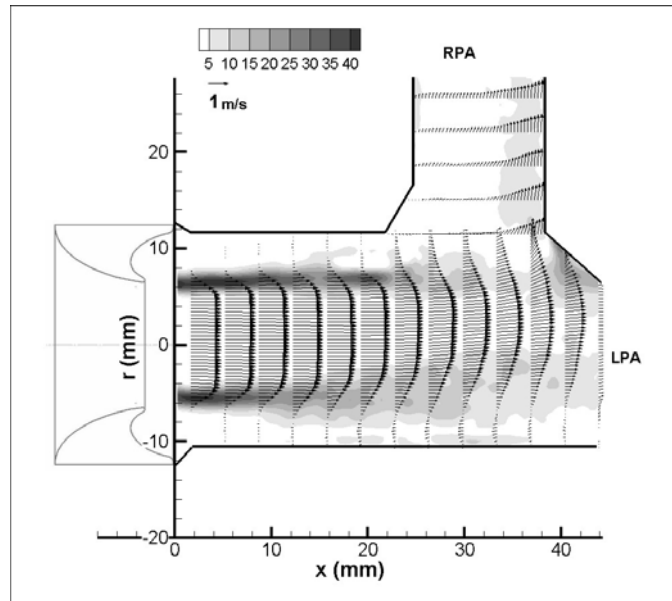
Figure 7.34: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR 6.1 mmHg/Lpm
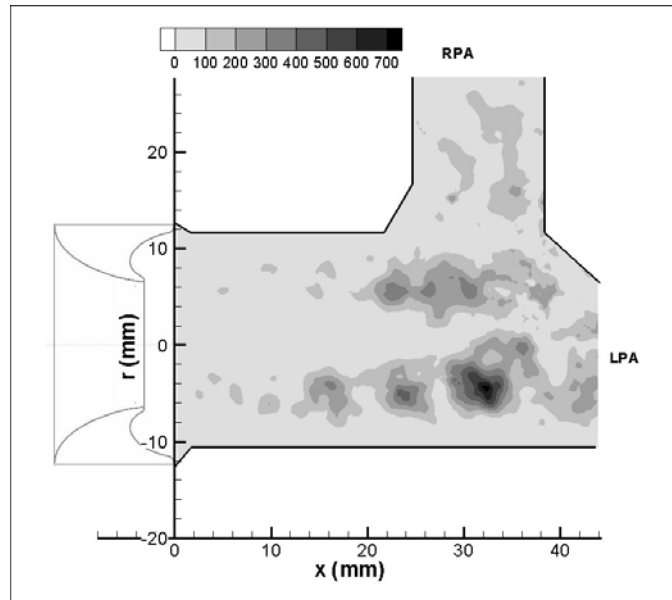

Figure 7.35: Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR = 6.1 mmHg/Lpm

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Late Diastole (t =750 ms)

The flow profile for late diastole is shown in Figure 7.38. Strong retrograde flow exists. The flow is uniform in the lower MPA and LPA and within the RPA. As the flow from the RPA reenters the main flow, flow separation occurs at the corner of the upper MPA and proximal RPA walls. This results in an area of stasis at the upper main pulmonary artery wall. The average flow speed is -0.199 in main artery with peak velocities of -0.443 m/s.

The hydraulic shear stress map for diastole is Figure 7.38. The peak stresses are around 11 dynes/cm^2 along the proximal wall in the right pulmonary artery. Overall, the viscous shear stresses are low. The RPA are washed back with the retrograde flow with wall stress at or above 5 dynes/cm^2. In the main and left artery branches, the wall stresses are between 1 and 5, so some areas are swept as well.

The mapping of the turbulent shear stresses in the flow 750 ms after the start of systole are in Figure 7.39. The retrograde flow from each artery is re-converging about 32 mm downstream and 4 mm above the MPA center as seen in Figure 7.38. This creates an area of mixing in which the RSS values reach 125 dynes/cm^2.

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Figure 7.36: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR 6.1 mmHg/Lpm
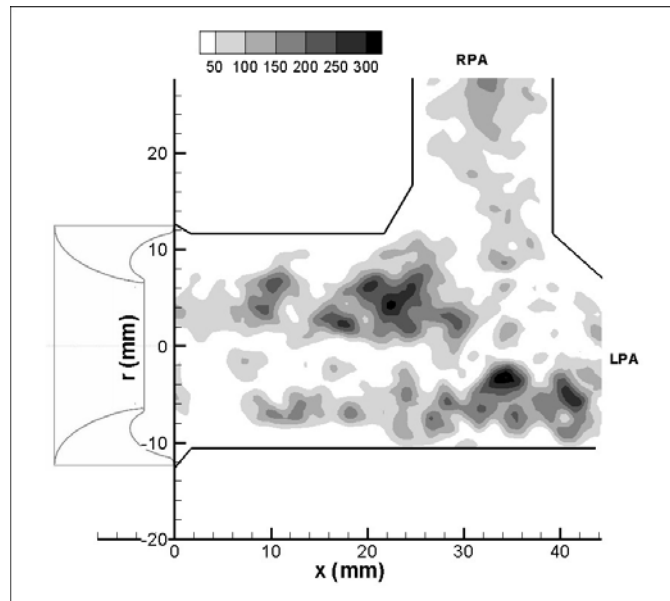
Figure 7.37: Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR = 6.1 mmHg/Lpm
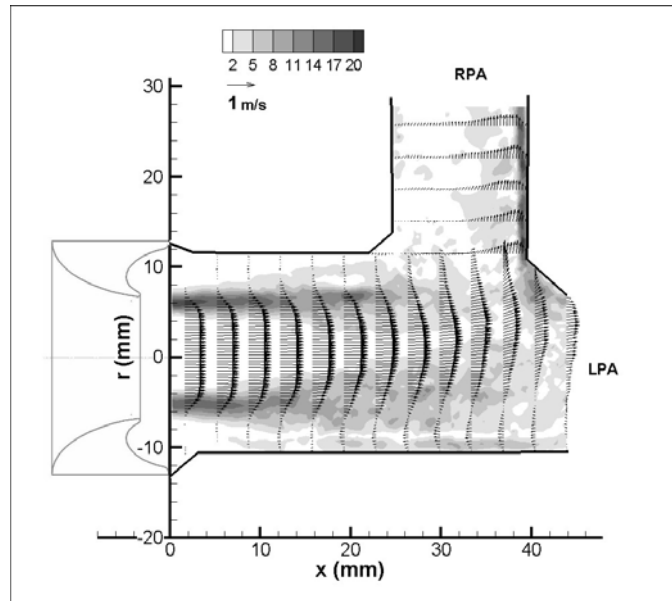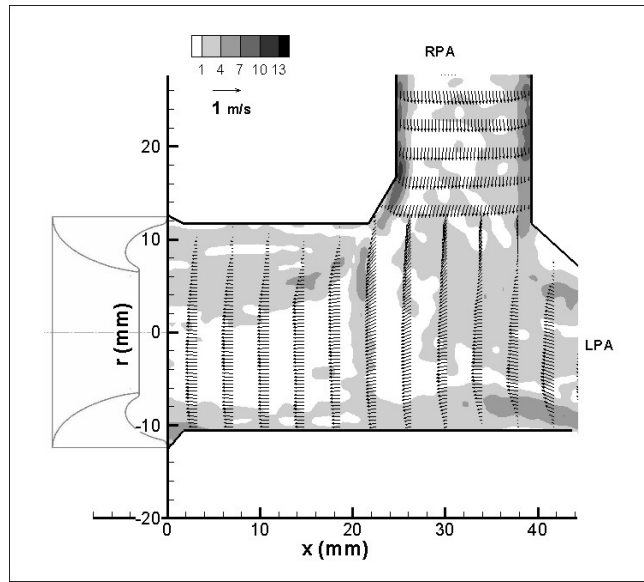
Figure 7.38: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR 6.1 mmHg/Lpm
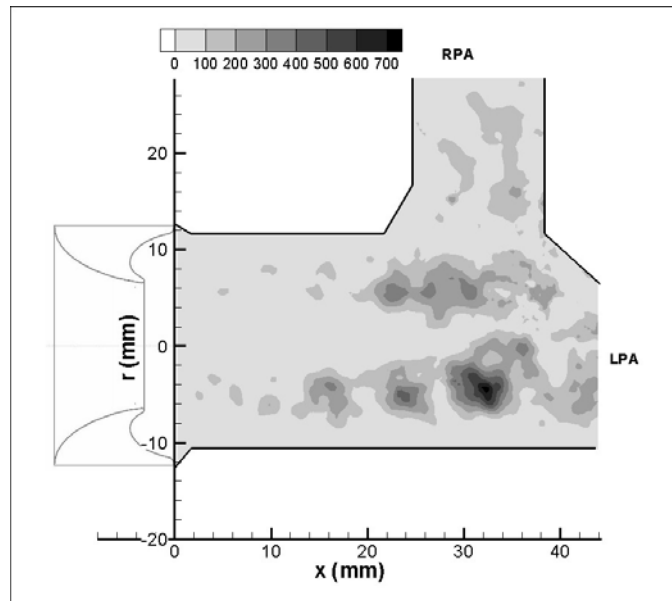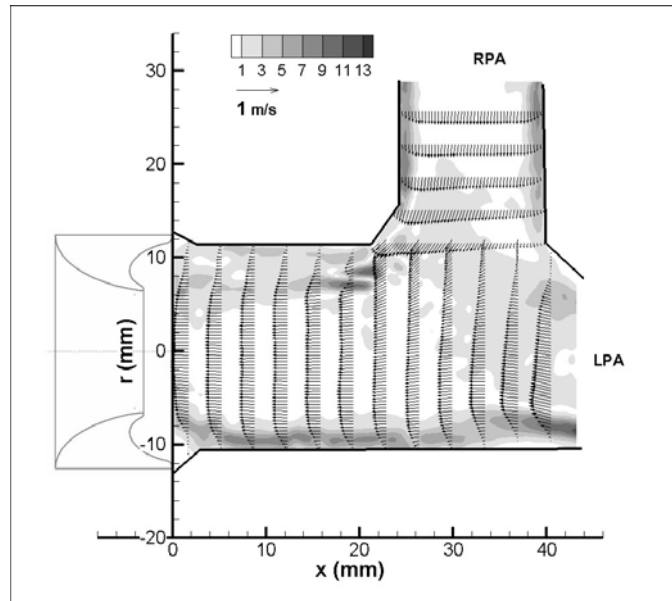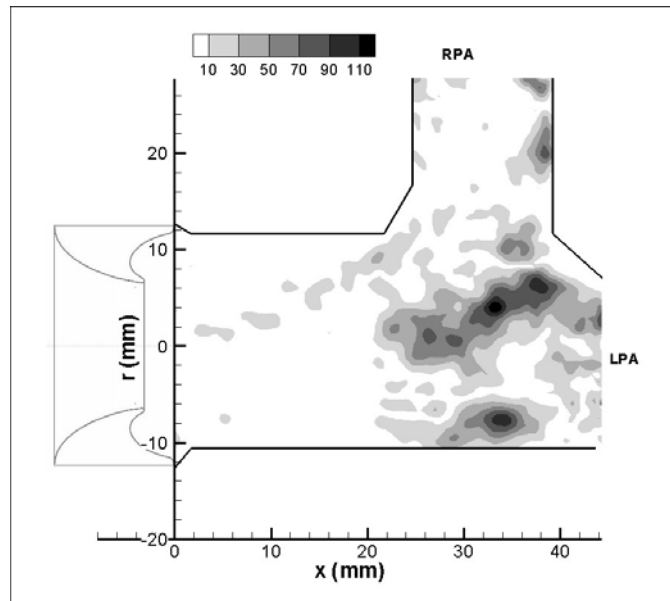

Figure 7.39: Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR = 6 .1mmHg/Lpm

<u>Back Channel Diode Results</u>

The back channel diode was tested under similar conditions as the open cusped diode; however, the system conditions were not exact matches for each case. Cases 1 and 4 will be presented for the backchannel diode valve. The results for both the central and offset planes will be featured for Case 1. The remaining descriptions are in Appendix B.

Case 1

At the low PVR and RF% settings for the back channel diode, the pressure and flow curves are shown in Figure 7.40. The PVR is 3.2 mmHg/Lpm and the RF% is 0.80%.

Early Systole (t =150 ms)

The flow and viscous shear stresses fields are shown in Figure 7.41. A developing jet is seen exiting the valve orifice. Flow separation occurs within the first 20 mm of the valve as indicated by a shear layer between the retrograde and antegrade flow. Beyond 20 mm, the flow is uniform into the left and right pulmonary arteries. The velocities in the MPA average 0.260 m/s and reach a maximum of 0.864 m/s.

The regions of the highest viscous shear stresses are along edge of the flow separation which is consistent with the indicated shear layer. The peak shear stresses are 26 dynes/cm^2. There are wall shear stresses of 5 - 6 dynes/cm^2 along the distal wall of the RPA.

The Reynolds shear stress field for the low PVR and RF% setting is shown in Figure 7.42. The RSS levels within the flow field measure 40 dynes/cm^2. At the valve exit, there is observed noise with point of RSS measuring as high as 225 dynes/cm^2. This may be a result of uncertainty in the velocity vector determination at this point in the field.

Peak systole (t = 350 ms)

The flow evolves into a developing jet as the cardiac cycle progresses to reach peak systole as a retrograde vortex moves across the artery walls (Figure 7.43). The core jet is well defined downstream of valve and into the LPA. The flow separates at the inner wall of the RPA branch, and a region of recirculation is present resulting in larger velocities along the outer wall. The peak velocity is 1.52 m/s and in the MPA, the average is 0.445 m/s.

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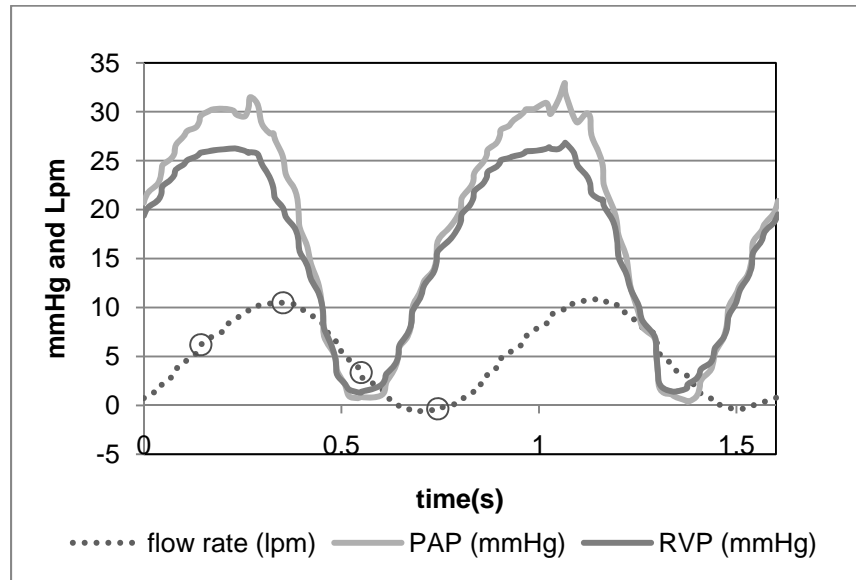
Figure 7.40: Pressure and flow curve for backchannel diode at PVR
= 3.2 mmHg/Lpm
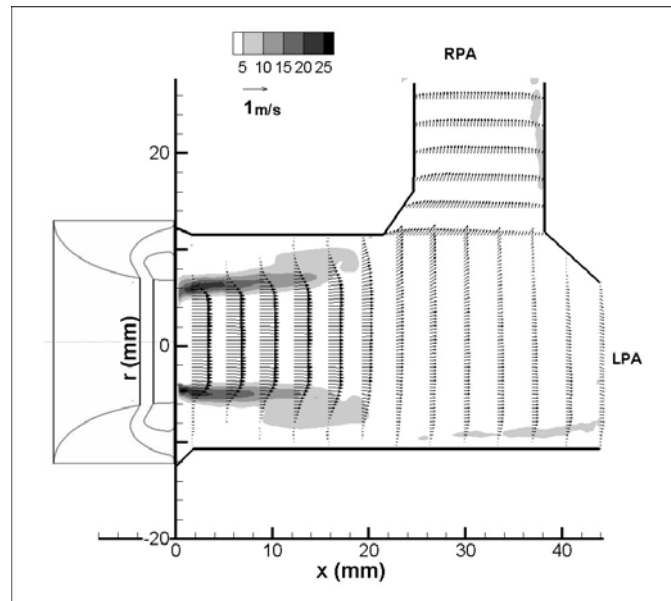
Figure 7.41: Central plane flow and viscous shear stress (dynes/cm^2) field for the
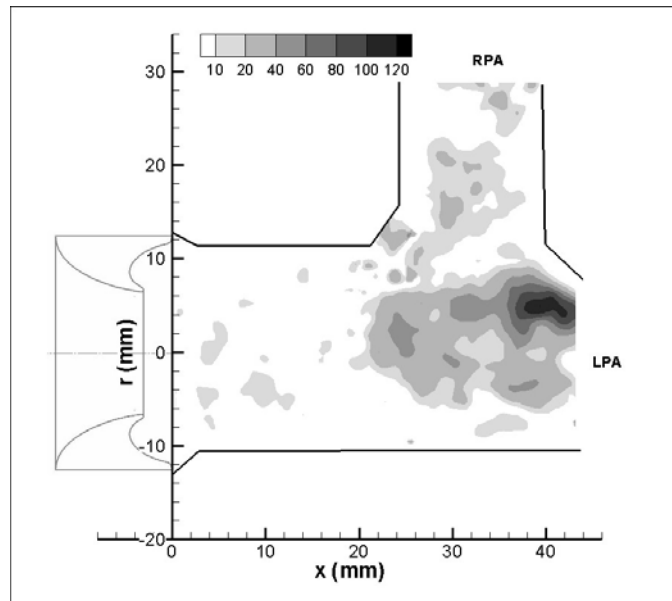backchannel diode at 150 ms after the start of systole for PVR = 3.2 mmHg/Lpm
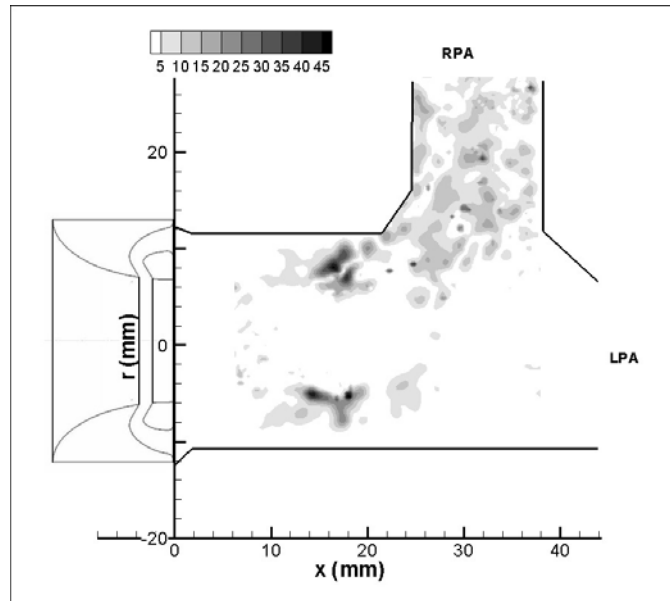
Figure 7.42: Reynolds shear stress field (dynes/cm^2) for the backchannel diode
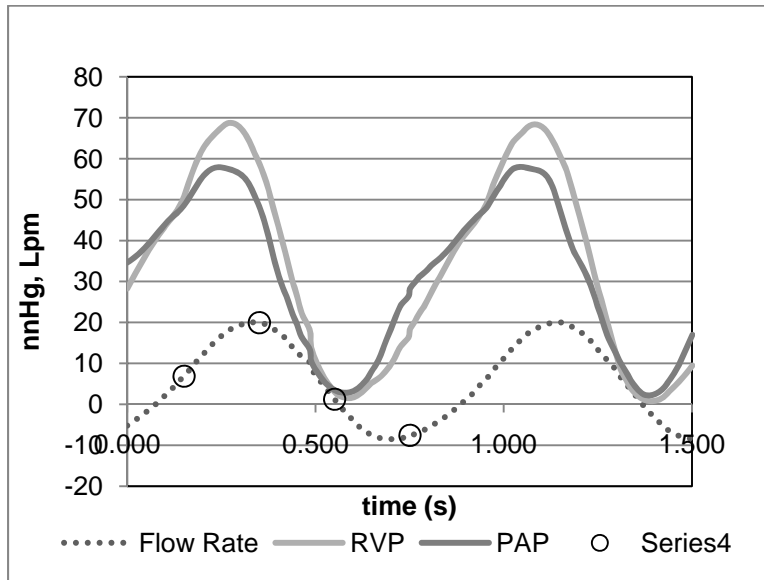at 150 ms after the start of systole for PVR = 3.2 mmHg/Lpm, central plane

Expectedly, the viscous shear stresses have increased as the shear layer has extended. Along the edges of the central core jet, the stresses peak 45 dynes/cm^2. The stresses along the distal RPA wall are as high as 27 dynes/cm^2. Along the lower MPA and into the LPA, the existence of retrograde flow leads to wall stresses of 10 - 14 dynes/cm^2.

Figure 7.44 shows the Reynolds shear at peak systole for Case 4. The regions of highest turbulence coincide with the areas of recirculation. One area, located about 6 mm off center in the lower MPA, has RSS values up to 750 dynes/cm^2. This area begins at 10 mm from the exit of the valve and extends into the LPA. At 6 mm above the centerline, there is another area of higher mixing. It begins about 20 mm from the valve exit. This

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is likely causes by the vortex that exists at the branch between the main and right pulmonary branches. The RSS values are as high as 225 dynes/cm^2 here. Finally, in the RPA branch, along the edge of weakening shear layer, there are turbulent stresses of 100 – 200 dynes/cm^2.

Mid Diastole (t = 550 ms)

Figure 7.45 maps the flow and bulk flow shear stresses during the mid diastole phase. The velocities measure less than one half of the peak systole velocities. The peak axial flow in the MPA is 0.629 m/s and the average is 0.163 m/s. There is still flow separation along the edges of the weakening jet.

The peak viscous shear stresses are 15 dynes/cm^2 at the edges of the jet structure (Figure 7.45). This region extends to about 25 mm downstream of the valve exit, as the jet entrainment fades. Also, the wall stresses are up to 10 dynes/cm^2 along the distal wall of the RPA.

The RSS field during mid diastole is shown in Figure 7.46. The highest turbulent shear stresses are 275 dynes/cm^2. They are located in the same area as did during peak systole, in the lower MPA and into the LPA. The other region of elevated RSS is near the branching of MPA and RPA flows.

The flow mapping of the diastolic flow field is shown in Figure 7.47. The flow velocities are near zero. The average within the MPA is 0.010 m/s with peaks up to 0.090 m/s.

The viscous shear stresses are also very low at this point in the cycle. The maximum shear stresses are between 3 and 4 dynes/cm^2. This is near the walls of the LPA and RPA.

Figure 7.48 shows the Reynolds shear stresses are very low during diastole. The peak RSS values are 40 dynes/cm^2.
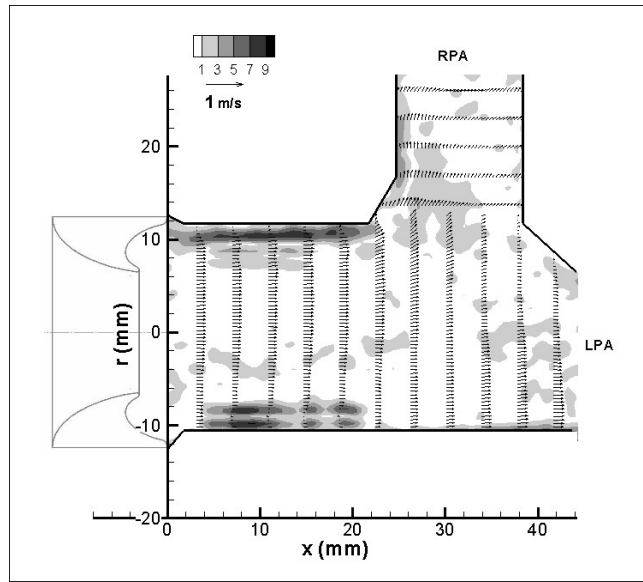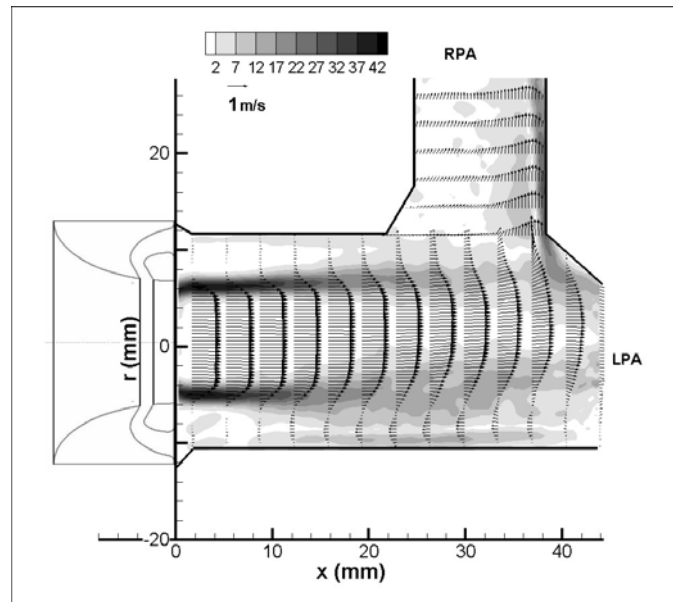

Figure 7.43: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 3.2 mmHg/Lpm
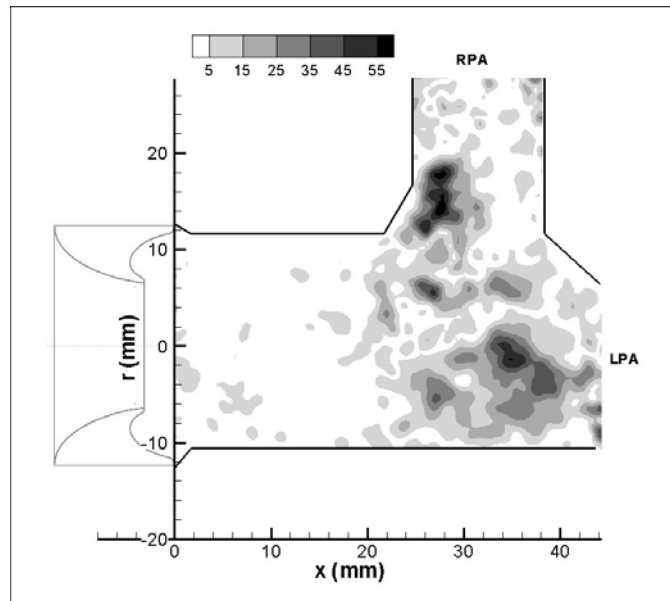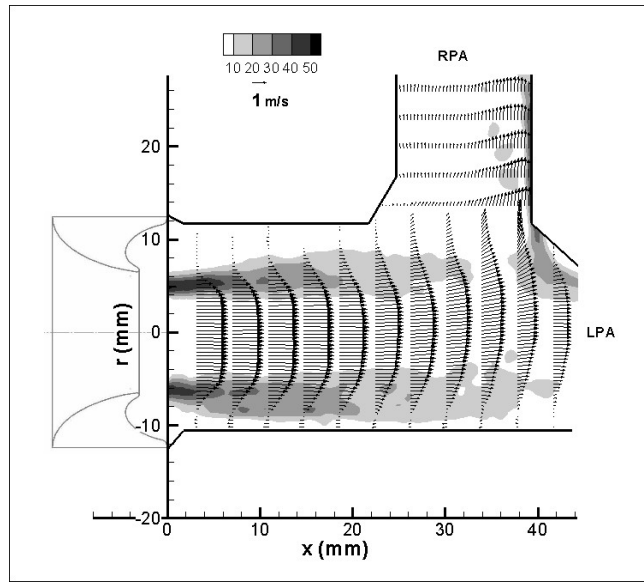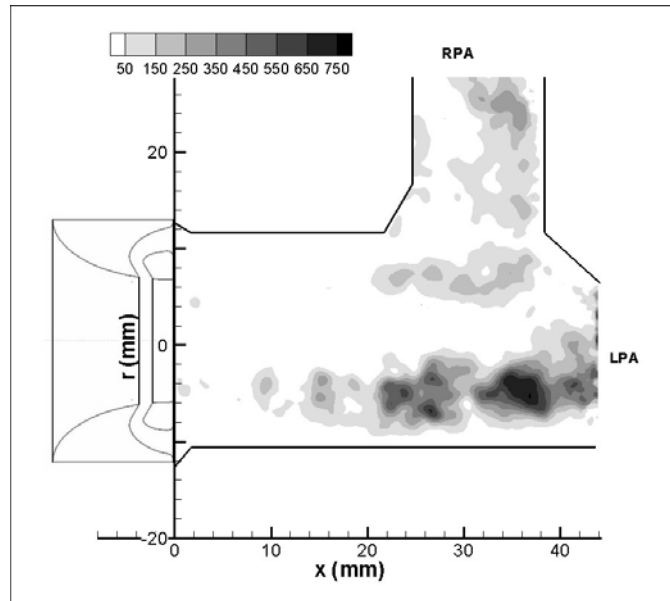
Figure 7.44: Reynolds shear stress field (dynes/cm^2) for the backchannel diode at 350 ms after the start of systole for PVR = 3.2 mmHg/Lpm, central plane
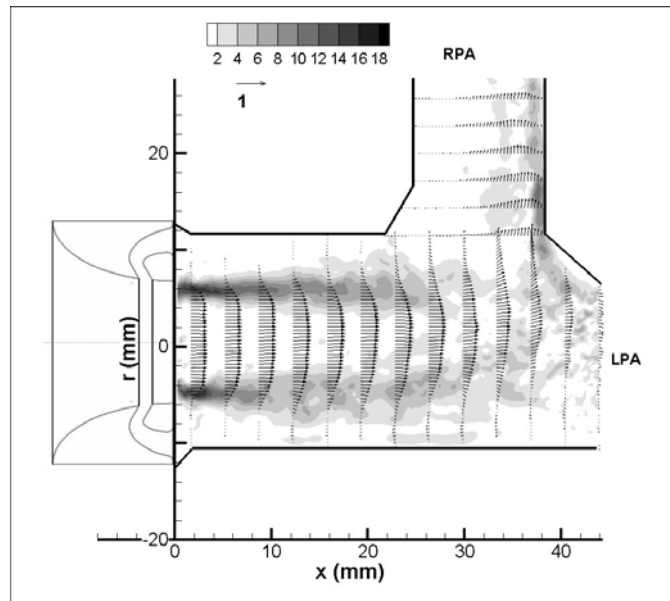
Figure 7.45: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR = 3.2 mmHg/Lpm
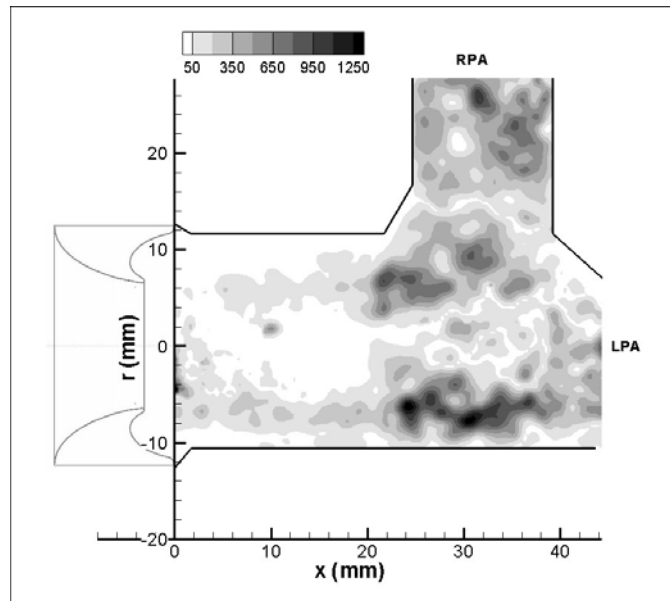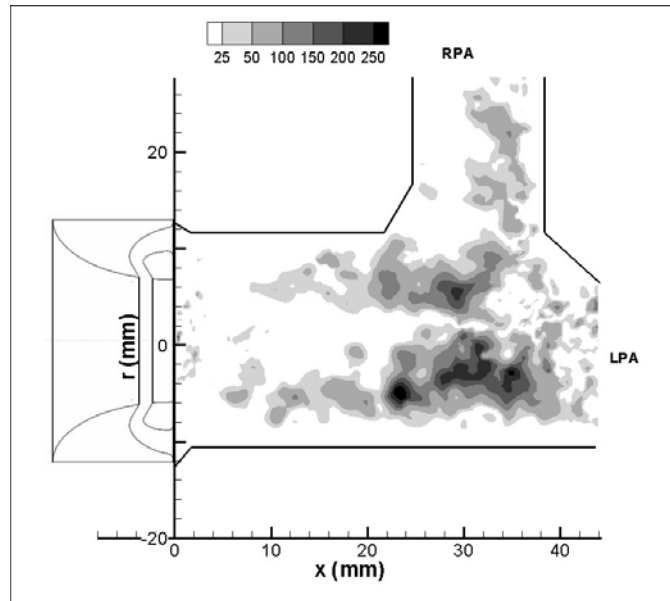
Figure 7.46: Reynolds shear stress field (dynes/cm^2) for the backchannel diode at 550 ms after the start of systole for PVR = 3.2 mmHg/Lpm, central plane
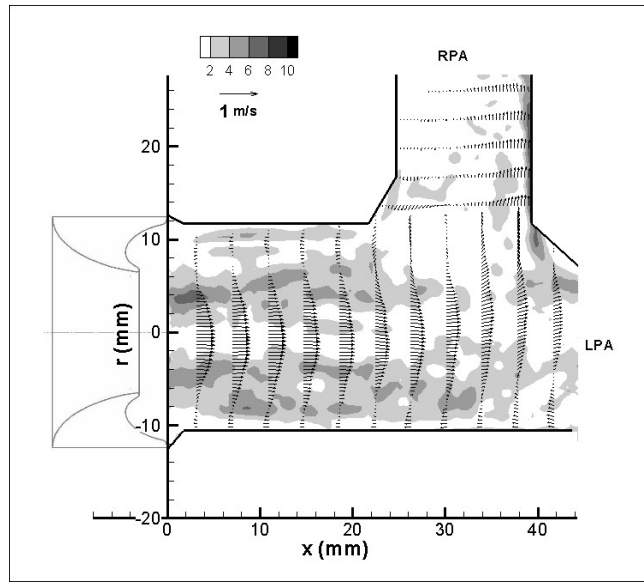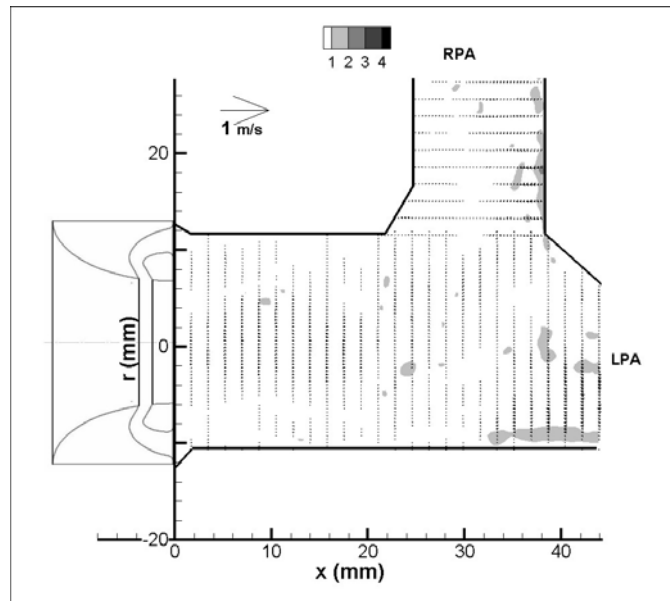

Figure 7.47: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 750 ms after the start of systole for PVR = 3.2 mmHg/Lpm

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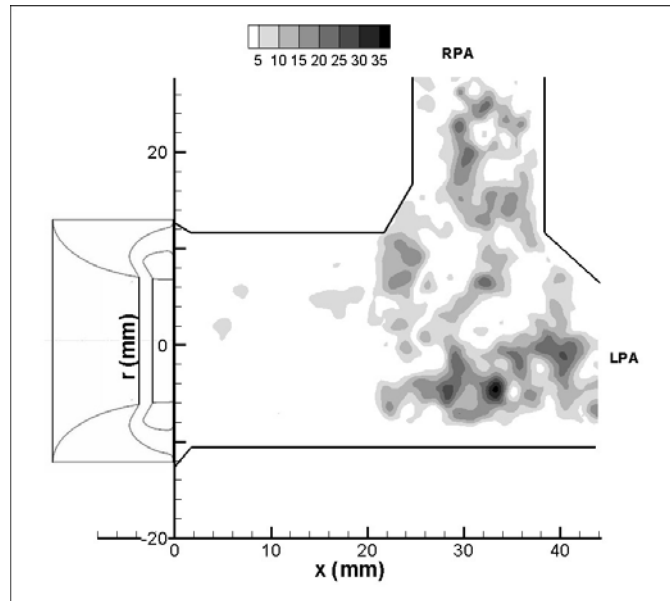
Figure 7.48: Reynolds shear stress field (dynes/cm^2) for the backchannel diode
at 750 ms after the start of systole for PVR = 3.2 mmHg/Lpm, central plane

Case 1 - Offset Plane

The flow profile in the offset plane at 150 ms after the start of systole is in Figure 7.49. The flow exiting the valve is still developing into a core jet. An area of recirculation occurs within the first 20 mm of the exit. The parabolic profile gives way to a more uniform profile at this location. The maximum velocity is 0.819 m/s, nearly 4 times the average velocity, 0.184 m/s. The viscous shear stresses are aligned with the edges of the jet. As the jet ends, the region of shear flares out in the radial direction as flow reversal takes place. The peak shear stress measures 20 dynes/cm^2 at the valve exit. Figure 7.50 shows the Reynolds shear stresses for the offset plane at t = 150 ms. The RSS values are low with none measuring higher than 15 dynes/cm^2.

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At peak systole the entrained jet is developing over the 22 mm range in Figure 7.51. The peak velocities in the central core jet are 1.493 m/s. The mean axial velocity is 0.311 m/s. The viscous shear stresses can also be seen in Figure 7.51. The peak shear stresses are along the edges of the jet and measure up to 35 dynes/cm^2. The shear layer flares out as the jet expands downstream. As with the central plane flow, the flow reattaches to the wall in the lower MPA 15 - 22 mm downstream. There is a resulting area of wall shear stresses of 9 dynes/cm^2. Figure 7.52 shows the RSS measurements at peak systole. The peak turbulent shear stresses are located 20 mm downstream just below the centerline. They are about 290 dynes/cm^2. The area of mixing occurs closer to the valve in the lower MPA as it was in the central plane.

The offset plane flow and bulk flow shear stress field is shown in Figure 7.53. The flow is decelerating and the jet structure is weakening. The peak flow velocities have slowed to 0.573 m/s and 0.107 m/s on average. The viscous shear stresses peak along the jet edges at 21 dynes/cm^2. There is still a region of higher shear stresses in the lower MPA where complete flow reversal has occurred. The turbulent shear stress mapping is in Figure 7.54. The peak turbulent stresses are 175 dynes/cm^2. This area is positioned along the center line about 10 mm downstream.
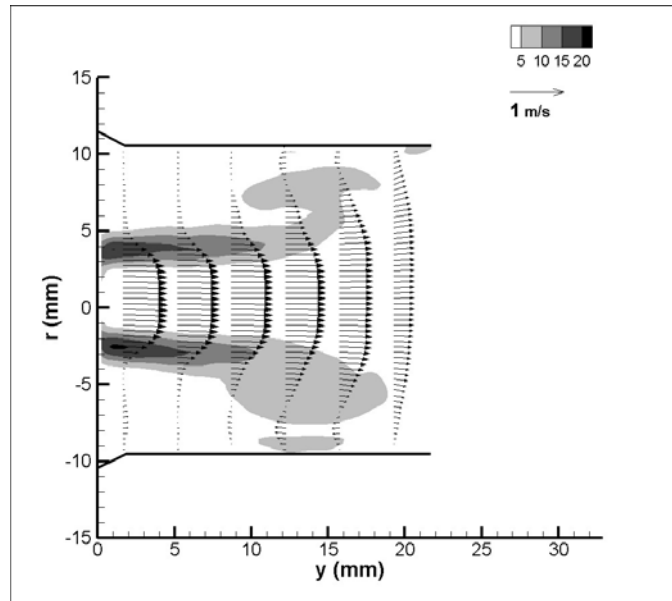
Figure 7.49: Offset plane flow and viscous shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm
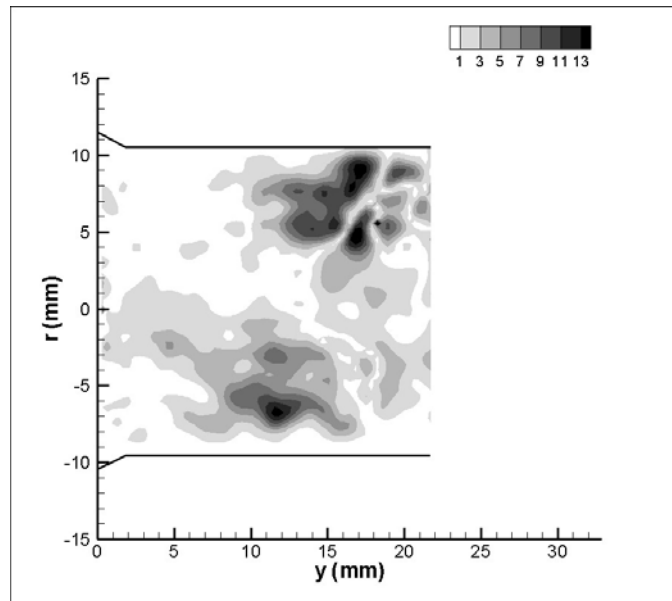
Figure 7.50: Offset Reynolds shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm

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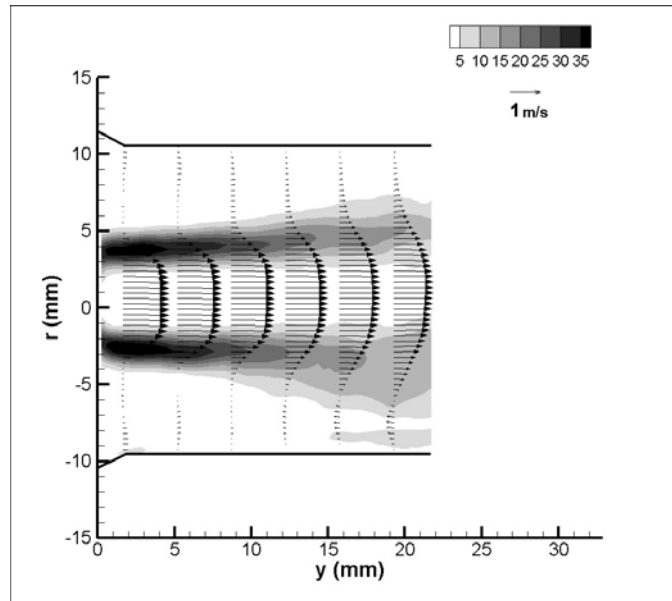
Figure 7.51: Offset plane flow and viscous shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm
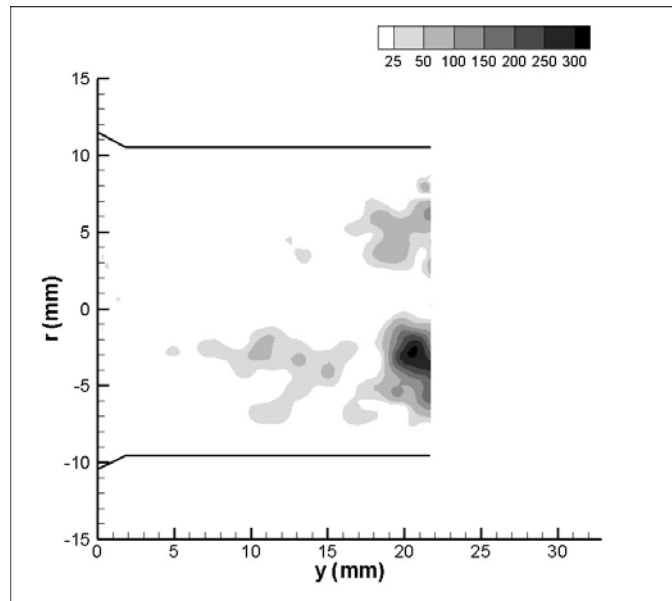
Figure 7.52: Offset Reynolds shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm

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Figure 7.55 maps the flow and viscous shear stresses for the offset plane during diastole. There is little to no flow at this time in the cardiac cycle. The peak and average flow velocity are 0.0183 m/s and -0.007 m/s, respectively. The viscous shear stresses are very low. The difference between the measured shear stresses and the measured noise is not significant. The turbulent shear stresses are also very low (Figure 7.56). The highest measured is 10 dynes/cm^2.
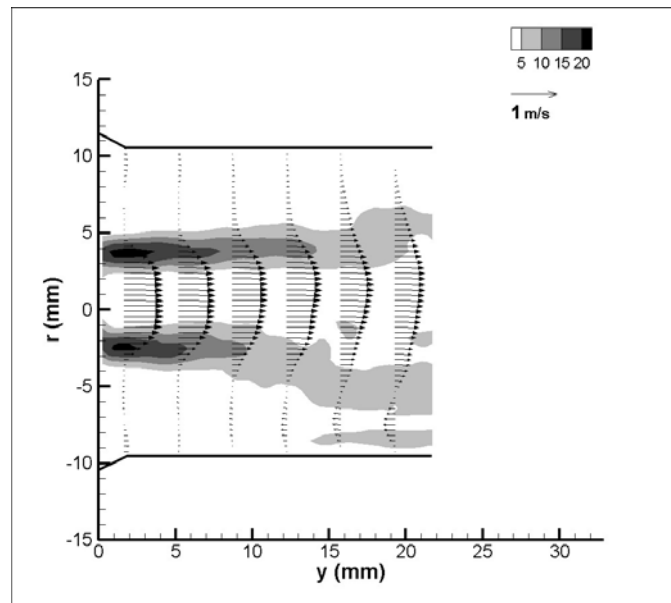
Figure 7.53: Offset plane flow and viscous shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm
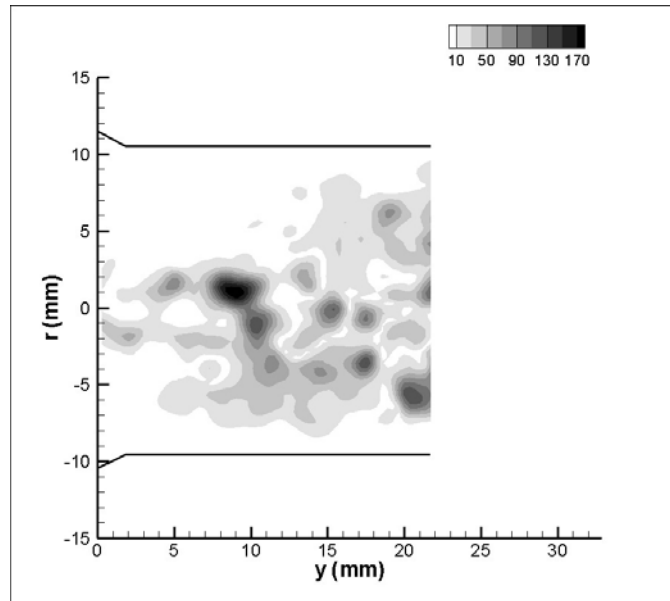
Figure 7.54: Offset Reynolds shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm
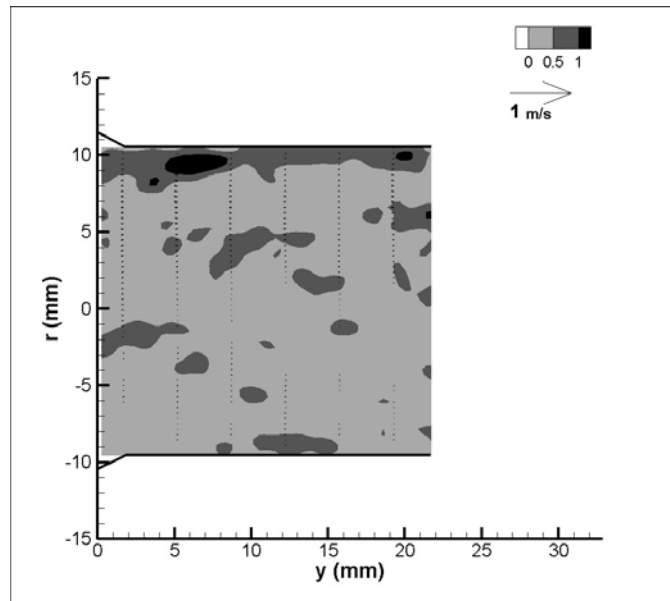
Figure 7.55: Offset plane flow and viscous shear stress (dynes/cm^2) field at 750 ms after start of systole for backchannel diode at PVR = 3.2 mmHg/Lpm

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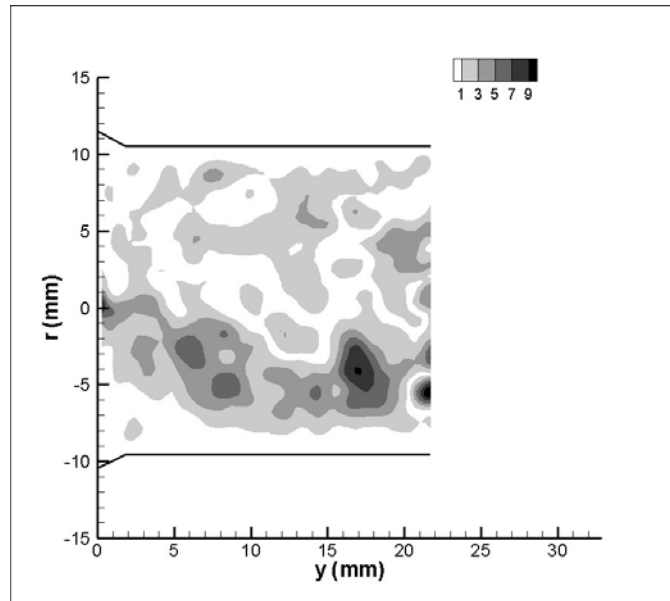
Figure 7.56: Offset Reynolds shear stress (dynes/cm^2) field at 750
ms after start of systole for backchannel diode at PVR = 3.2
mmHg/Lpm

Case 3 – Offset Plane

Early Systole (t =150 ms)

The offset flow and viscous shear stress fields (Figure 7.57) are similar to central
plane flow field. The flow profile is uniform and the highest viscous shear stresses are
along the walls. The average and peak velocities are 0.057 m/s and 0.181 m/s,
respectively. The peak wall stresses are about 5 dynes/cm^2.

Much of the mixing that occurs 150 ms into the cardiac cycle takes place in the
area downstream of this field of view (where flow is branching off into 2 directions).
Therefore, the RSS measurements are very low in the first 22 mm downstream of the
valve exit as seen in Figure 7.58. The measurements are less than 5 dynes/cm^2.

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Peak systole (t = 350 ms)

Figure 7.59 shows the off plane flow and viscous shear stress field during peak systole. As with the central plane, there is a well defined jet structure. Expectedly, it is narrower than the central plane jet. The maximum flow speed is 2.07 m/s and the average is 0.506 m/s. There is an area of recirculation in the below the centerline. The areas of highest bulk flow shear stresses border the entrained jet. The peak stresses are 55 dynes/cm^2 and are just at the valve exit. The wall shear stresses along the lower MPA are between 10 - 15 dynes/cm^2.

The developed area of recirculation in the lower MPA created an area of turbulence that can be seen in Figure 7.60. At -5 mm below the centerline, there is a region of elevated turbulent shear stresses. The peak RSS measurements are around 400 dynes/cm^2. In general, the Reynolds shear stress values are similar those in the first 22 mm of the central plane data.

Mid diastole (t = 550 ms)

Figure 7.61 is the off plane view of the flow and viscous shear stresses for the mid diastole phase. The central flow stream is weakening. The maximum and average velocities have decreased to 0.975 m/s and 0.224 m/s, respectively. The vortical structure is still present between the jet and the lower wall. There shear layers generated by the flow separation leads to the peak viscous shear stresses of 23 dynes/cm^2 along the edges of the jet. Figure 7.62 maps the turbulent shear stresses. The higher RSS measurements

are positioned in the area of the recirculation where mixing occurs. The peak Reynolds shear stress is 450 dynes/cm^2.

Late Diastole (t = 750 ms)

The diastolic flow profile is shown in Figure 7.63. The average flow velocity is -0.092 m/s. The peak velocity is -0.213 m/s. The uniform retrograde flow allows for a complete wash of the artery the walls as it did in the central plane. The wall shear stresses for this case measure less than 5 dynes/cm^2. The overall Reynolds shear stresses during diastole in the off plane field of view are low (Figure 7.64) at less than 25 dynes/cm^2.
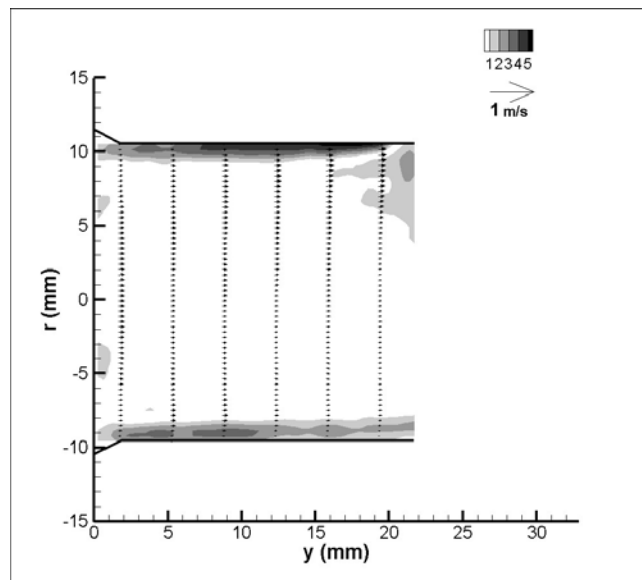
Figure 7.57: Offset plane flow and viscous shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
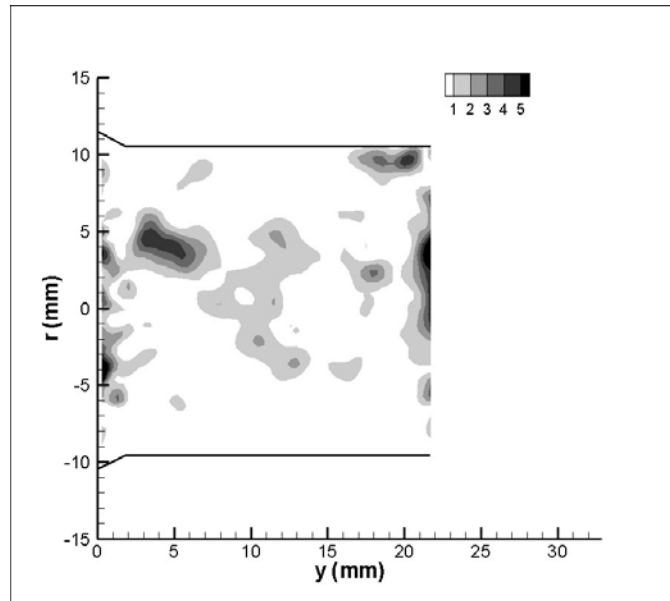
Figure 7.58: Offset Reynolds shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
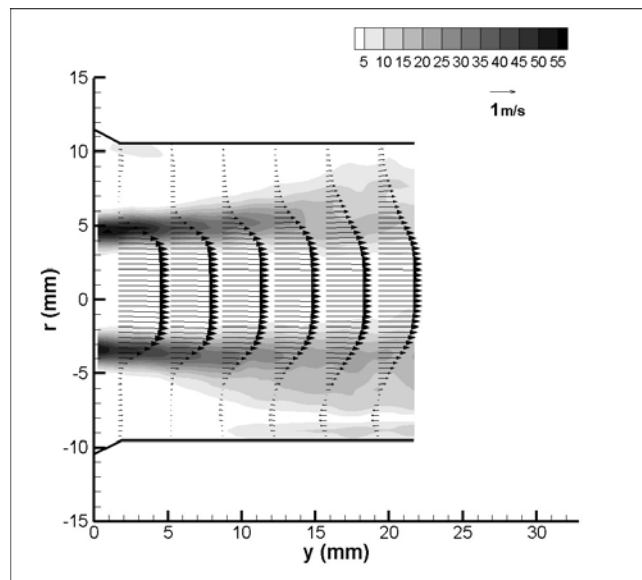
Figure 7.59: Offset plane flow and viscous shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
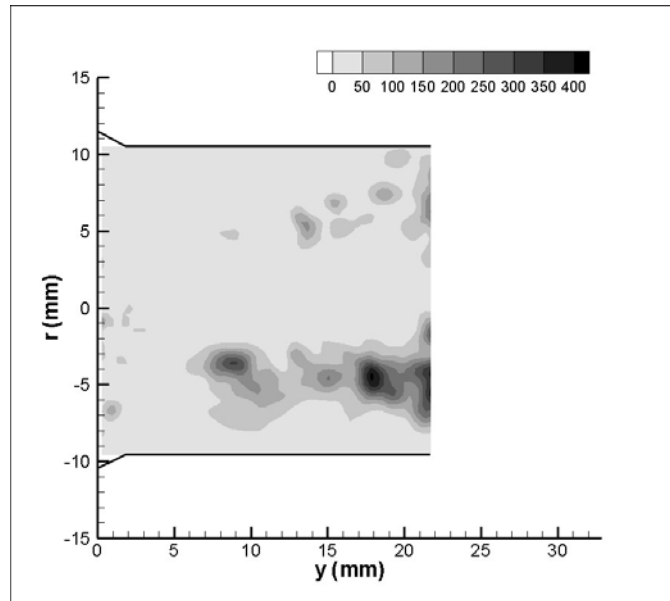
Figure 7.60: Offset Reynolds shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
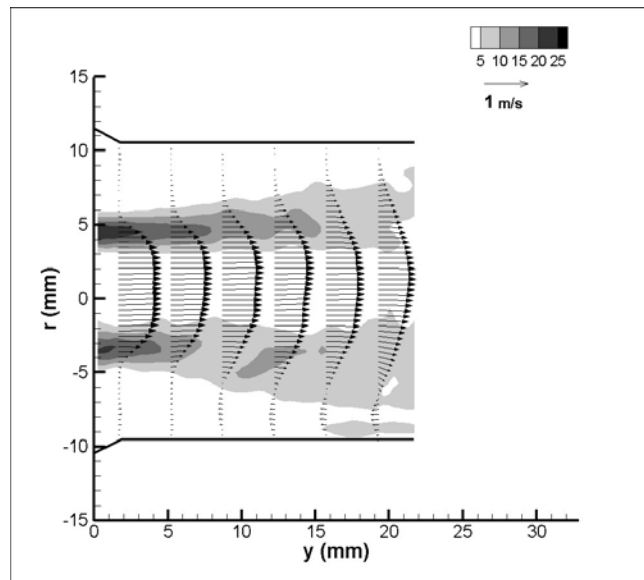
Figure 7.61: Offset plane flow and viscous shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
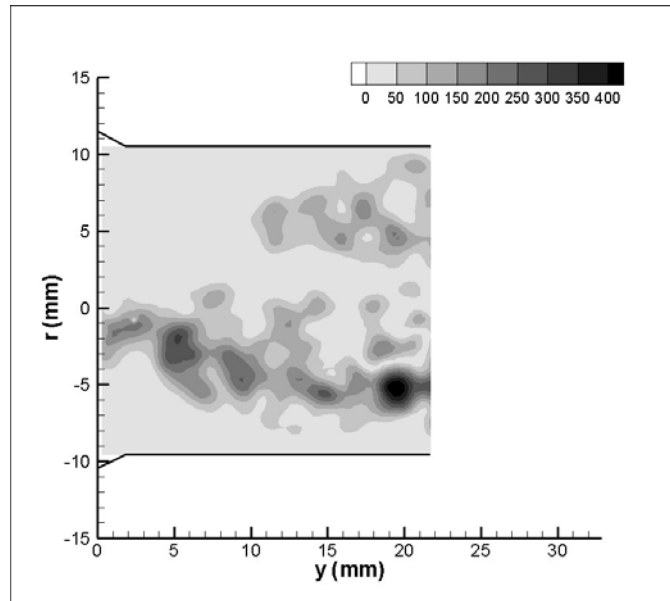
Figure 7.62: Offset Reynolds shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm
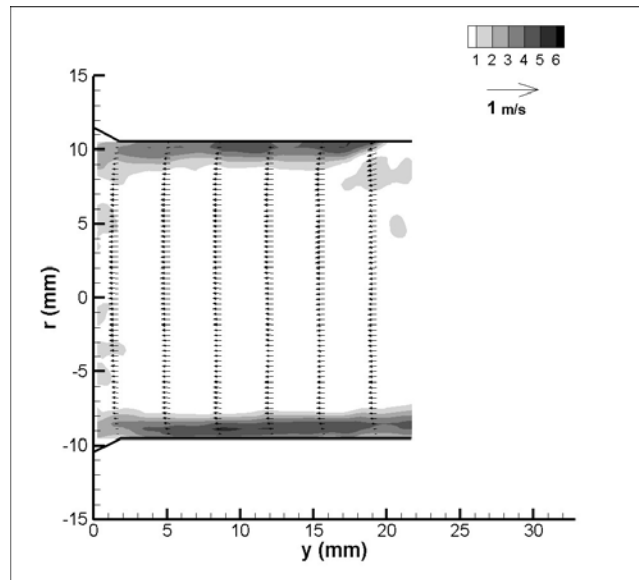
Figure 7.63: Offset plane flow and viscous shear stress (dynes/cm^2) field at 750 ms after start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm

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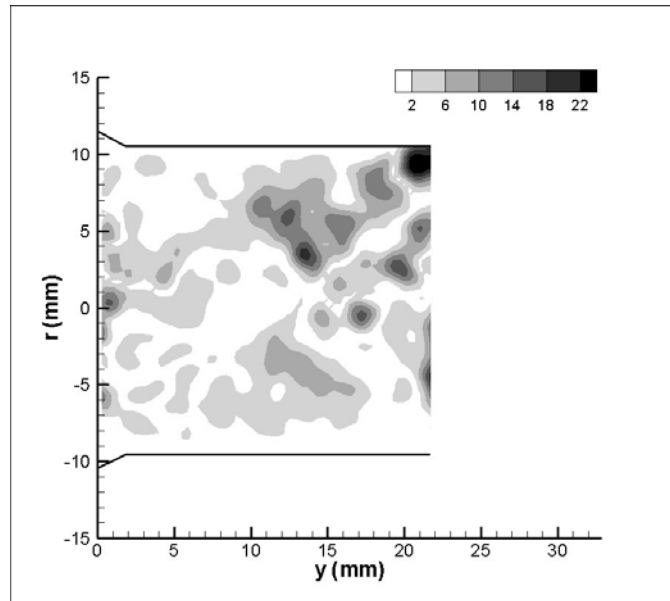
Figure 7.64: Offset Reynolds shear stress (dynes/cm^2) field at 750 ms after
start of systole for backchannel diode at PVR = 5.1 mmHg/Lpm

Case 4

The final condition under which the backchannel diode was tested was at a PVR =
6.85 mmHg/Lpm and a RF% = 30.5%. The pressure and flow curves are shown in
Figure 7.65.

Early Systole (t = 150 ms)

The velocity and viscous shear stress profile for the diode valve with a
backchannel is mapped in Figure 7.66. The flow is unsettled at this early point in the
cardiac cycle. Flow from the two branches is mixing in the MPA. There is an area of
recirculation that extends from the 5 mm to 22 mm downstream of the valve. The

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average velocity in the MPA was near zero at 0.002 m/s, and the peak velocity was 0.153 m/s.

The resulting viscous shear stresses from this flow field are also shown in Figure 7.66. The measured shear stresses are lower than 5 dynes/cm^2. The peak is 4.7 dynes/cm^2 along the wall of the upper MPA and the lower LPA.

Figure 7.67 shows the Reynolds shear stresses at 150 ms after the start of the cycle. The locations of higher RSS are located between 22 and 40 mm downstream where the flow from the RPA mixes with the flow in the MPA and LPA. Overall, the RSS values are less than 68 dynes/cm^2.
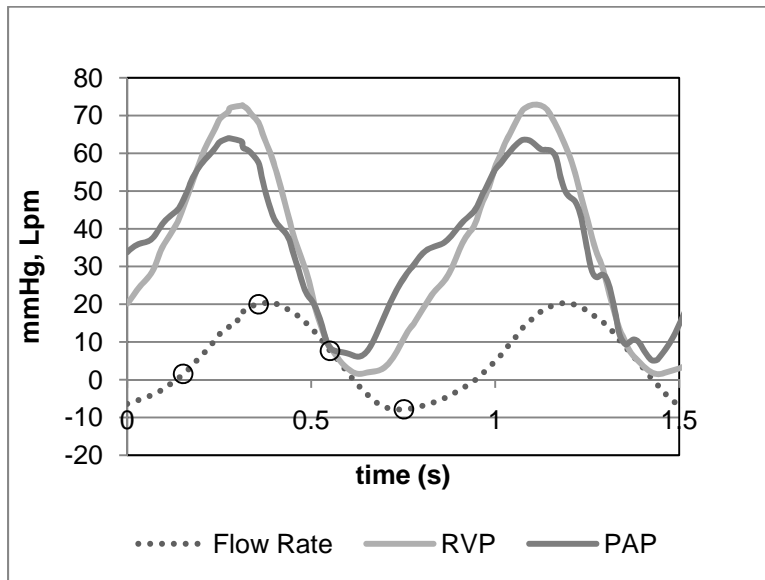
Figure 7.65: Pressure and flow curve for backchannel diode
at PVR = 6.9 mmHg/Lpm

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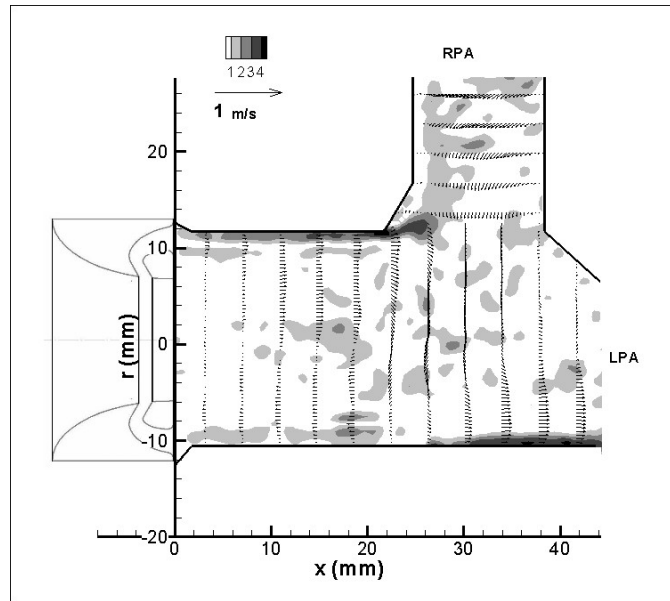
Figure 7.66: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR 6.9 mmHg/Lpm
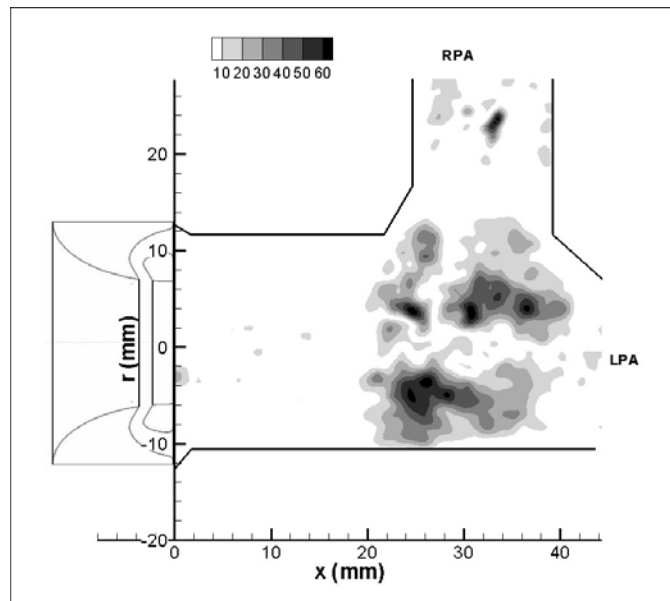
Figure 7.67: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR = 6.9 mmHg/Lpm

Peak Systole (t = 350 ms)

At peak systole, the behavior of the flow is same as it was for the previous cases. An entrained jet emerges from the valve and travels downstream (Figure 7.68). A higher flow rate exists, therefore the velocities are higher. There are vortical structures surrounding the jet. The flow in the RPA is still skewed towards the distal wall, but the velocity gradient is not as great as it was in cases 2 and 3 for the backchannel diode (Figure B.39, Figure B.56). The average axial velocity in the main artery is 0.723 m/s. The peak axial velocity is 2.30 m/s, at the exit of the jet.

The bulk flow shear stresses are also shown in Figure 7.68. Expectedly, the peak shear stresses are located along the edges of the central jet. The peak shear stress at 350 ms into the cardiac cycle measures 64 dynes/cm^2. The wall stresses on the distal RPA wall range between 19 - 38 dynes/cm^2. At the lower wall in the main and into the left artery branch, the wall stresses are as high as 16 dynes/cm^2.

Figure 7.69 shows the turbulent shear stresses for this case at peak systole. The point of maximum turbulent stresses (1716 dynes/cm^2) is in the LPA at the end of the area of recirculation. Within this same vortical structure, the stresses are around 1000 dynes/cm^2. The RSS values reach up to 722 dynes/cm^2 where the MPA flow begins to diverge into the RPA.

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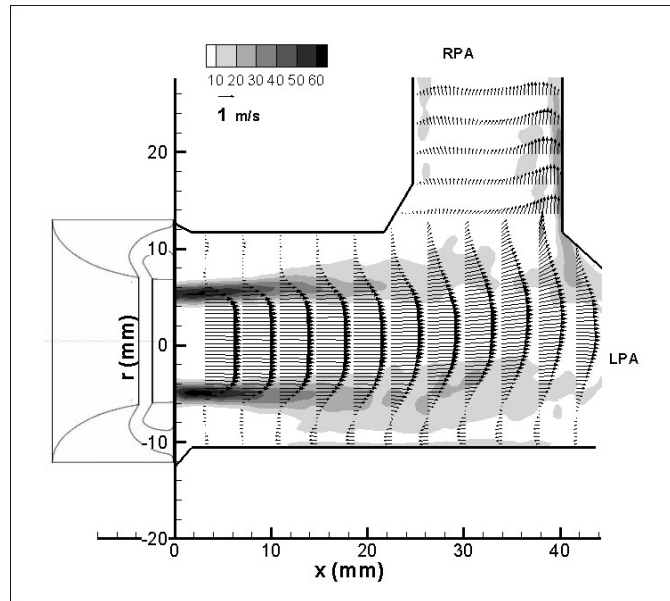
Figure 7.68: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR 6.9 mmHg/Lpm
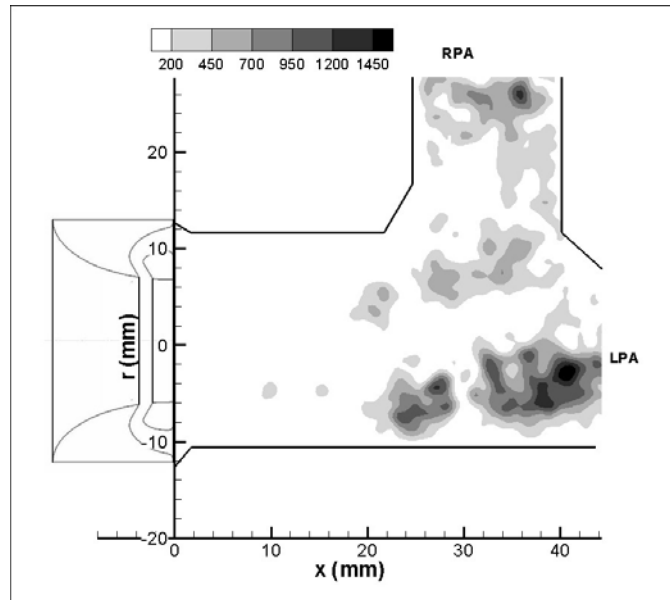
Figure 7.69: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 6.9 mmHg/Lpm

Mid Diastole (t = 550 ms)

Figure 7.70 is the flow and viscous shear stress field at 550 ms after the start of systole. It shows a weakening jet structure bounded on the top and bottom by areas of recirculation. The flow in the RPA has begun to reverse course. A region of recirculation has formed in the RPA, and retrograde flow is present at the proximal RPA wall. The average and peak axial velocities in the MPA are 0.136 m/s and 0.567 m/s, respectively.

The peak shear stresses are seen to occur at the jet edges just as the valve exit. They measured 10.2 dynes/cm^2. The wall stresses are between 2 and 5 dynes/cm^2 along the walls of the MPA, where the flow has reattached. For the distal RPA wall, the stresses are about 3-8 dynes/cm^2.

The RSS values range up to 362 dynes/cm^2 (Figure 7.71). The highest turbulent shear stresses are located in the area where the flow from the RPA mixes with the flow in the MPA, about 28 mm downstream and 7 above the center of the MPA. Also, in the lower MPA, the elevated turbulent shear stresses coincide with the point where the flow separation ends.

Late Diastole (t =750 ms)

The regurgitant fraction for this case was 30.5%. Thus, at diastole, strong retrograde flow is observed in the velocity field (Figure 7.72). The flow is evenly

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distributed in the MPA as well as the branches. The flow speeds have a maximum of -0.928 m/s and an average of -0.296 m/s.

As a result of the uniform flow profile the wall stresses are higher than within the flow field. The peak stresses of 12.5 dynes/cm^2 during the diastolic phase are seen along the lower part of the MPA. The right pulmonary artery walls are washed well as the shear stresses are between 5 and 10 dynes/cm^2. Also, stresses of similar magnitude result from the flow as it is reentering the valve.

Figure 7.73 shows the Reynolds shear stresses that range between 0 and 196 dynes/cm^2. The mixing of the two secondary flows creates a higher level of disturbance.
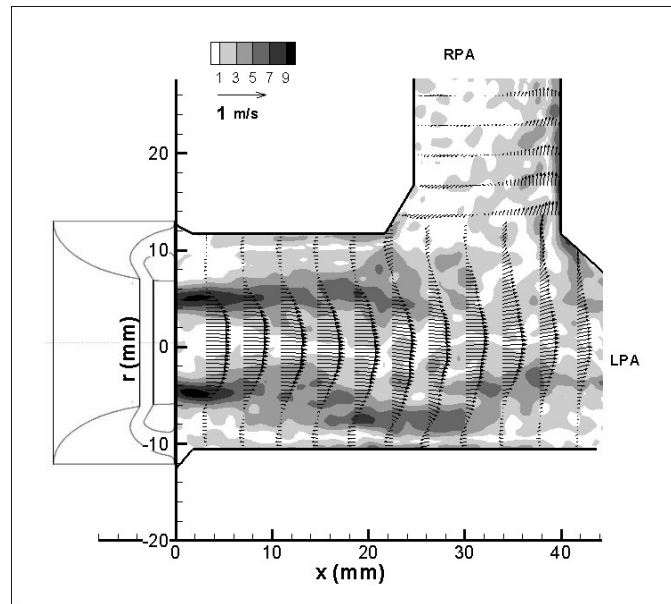
Figure 7.70: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR 6.9 mmHg/Lpm

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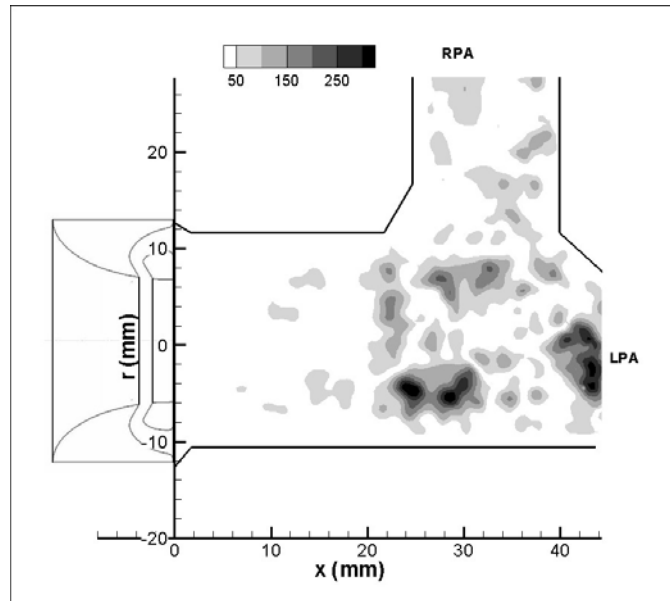
Figure 7.71: Reynolds shear stress (dynes/cm^2) field for the backchannel
diode at 550 ms after the start of systole for PVR = 6.9 mmHg/Lpm
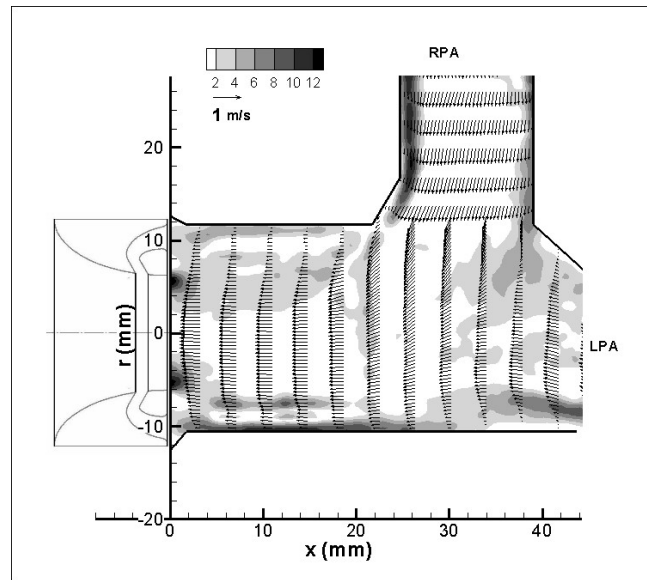
Figure 7.72: Central plane flow and viscous shear stress (dynes/cm^2) field for
the backchannel diode at 750 ms after the start of systole for PVR 6.9
mmHg/Lpm

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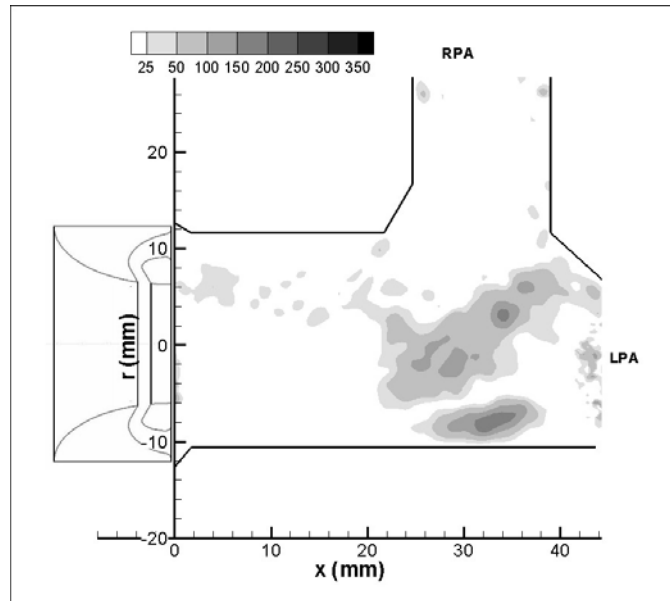
Figure 7.73: Reynolds shear stress (dynes/cm^2) field for the backchannel diode
at 750 ms after the start of systole for PVR = 6.9 mmHg/Lpm

Comparison of Backchannel and Open Cusped Diode Valves

Both valve designs were tested at similar physiological conditions; thus, their hemodynamic performances can also be compared. In general, the valves had pressure gradients and regurgitant fractions following the earlier findings; the backchannel diode valve had lower RF% for some levels of PVR. The most noticeable difference is at for PVR ~ 4mmHg/Lpm and PVR = 5.1. The backchannel diode experiences RF% levels that are 50% and 20% lower than that of the open cusped diode valve. Only one data point was taken at each PVR; therefore, no statistical inference can be about this comparison.

Table 7.1 summarizes the average and peak velocities, peak viscous shear stresses and the peak RSS for both valves at PVR = 3 mmHg/Lpm. At the lowest PVR, the backchannel diode has a more defined jet structure at 150 ms after the start of systole. The corresponding viscous shear stresses along the edges of the jet are higher for the backchannel diode than the open cusped. The Reynolds shear stresses are more than 15 times higher for the backchannel at this point as a result of the more active flow. At peak systole the peak flow speeds are higher for the backchannel diode (1.52 m/s versus 1.28 m/s). All other measurements were similar. As a result, the viscous shear stresses occur in a similar pattern with higher magnitudes for the backchannel diode. The Reynolds shear stress fields are similar for each valve as well. During mid diastole and diastole, the flow behavior for both valves is comparable.

Table 7.1. Comparison PIV Results for Backchannel (PVR = 3.2 mmHg/Lpm) and Open Cusped (PVR = 3.1 mmHg/Lpm) Diode Valves

Time (ms)	Open Cusped Diode				Backchannel Diode			
	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)
150	0.150	0.080	3.7	15	0.864	0.260	29.9	225
350	1.280	0.410	32.2	600	1.52	0.445	43.5	735
550	0.600	0.186	12.9	300	0.629	0.163	15	290
750	-0.072	-1.89	4.4	50	0.090	0.010	4	40

As the resistance level increased, the comparison between the open cusped and backchannel designs did not change much from the first case. The jet flow exiting the

backchannel diode valve was more defined at 150 ms after systole start than for the open cusped diode. The flow for the open cusped valve is still transitioning from retrograde to antegrade. The maximum RSS for the backchannel valve is almost 3 times higher than the maximum for the open cusped diode at peak systole (Table 7.2). During diastole, uniform reverse flow profile is better developed with higher flow speed in the open cusped diode flow field. This coincides with the higher negative flow rate and RF% that the open cusped valve experiences.

Table 7.2. Comparison PIV Results for Backchannel (PVR = 4.3 mmHg/Lpm) and Open Cusped (PVR = 4.2 mmHg/Lpm) Diode Valves

Time (ms)	Open Cusped Diode				Backchannel Diode			
	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)
150		-0.330	6	78	0.501	0.111	5.0	23
350	1.32	0.504	35	268	1.78	0.517	51.5	800
550	0.824	0.286	17.6	350	0.794	0.228	20.6	540
750	-0.413	-0.149	8.6	60	-0.186	-0.052	4.0	45

For the third PVR level, the flow rate curves generated by the open cusped and backchannel valves have different shapes. The highest flow rate for the open cusped diode take places 450 ms after the start of systole instead or 350 ms. During early systole, the flow for the backchannel diode is fairly uniform antegrade flow while the flow through the open cusped diode is reversing direction. In fact, the average axial velocities describe this more aptly. The average velocity for the open cusped design is -

0.186 m/s as opposed to 0.059 m/s for the backchannel diode. All the velocities and shear stresses are listed in Table 7.3. When comparing the flow patterns at peak systole, the flow velocities and shear stresses are higher for the backchannel diode. Yet, both peak RSS values are around 1100 dynes/cm^2. During mid diastole, the flows have similar shear stress measurements and speeds. However, at late diastole, the valve with the open cusp has reverse flow vectors twice that of the backchannel diode valve. This is because of the open cusped had more regurgitant flow than the other valve design at this PVR.

Table 7.3. Comparison PIV Results for Backchannel (PVR = 5.1 mmHg/Lpm) and Open Cusped (PVR = 5.1 mmHg/Lpm) Diode Valves

Time (ms)	Open Cusped Diode				Backchannel Diode PVR = 5.1 mmHg/Lpm			
	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)
150	-0.186	-0.208	5.0	135	0.196	0.059	3.6	55
350	1.63	0.576	45.0	736	2.07	0.611	63.1	1150
450	1.65	0.583	45.2	1130				
550	0.881	0.282	23.1	760	0.981	0.283	20.0	750
750	-0.500	-0.196	8.3	121	-0.273	-0.088	8.0	76

Finally, the flow fields for both diode valve designs are compared at a PVR of roughly 6 mmHg/Lpm. The summary table is shown in Table 7.4. The regurgitant fraction for both valves measure 30%. During early systole, the flow through the backchannel diode valve is reversing its motion. For the open cusped, there is uniformly distributed forward flow. The magnitudes of the bulk flow shear stresses and turbulent shear stresses are similar. At peak systole, the backchannel diode has a tighter jet leaving

its exit. The shear stresses are slightly higher for the backchannel diode flow than the open cusped diode flow. At mid diastole, the viscous shear and turbulent shear stress peak value are comparable. The flow profiles are both uniform retrograde flow for both valve designs, while the hydraulic and RSS magnitudes are similar.

Table 7.4. Comparison PIV Results for Backchannel (PVR = 6.9 mmHg/Lpm) and Open Cusped (PVR = 6.1 mmHg/Lpm) Diode Valves

Time (ms)	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)	u_{peak} (m/s)	u_{avg} (m/s)	τ_{max} (d/cm^2)	RSS_{max} (d/cm^2)
150	0.289	0.115	9.1	65	0.153	0.002	5.1	68
350	2.37	0.860	55.3	1520	2.30	0.723	64.4	1720
550	0.487	0.124	9.2	340	0.567	0.136	10.2	362
750	-0.443	-0.199	11.1	125	-0.928	-0.296	12.1	196

Overall, the flow patterns of the both designs behaved similarly. Central jet flow emerges from the valve and travels downstream into the left pulmonary artery. The jet structures are entrained by rolling vortical structures. The flow begins to reattach to the artery walls at varying locations depending on the PVR. The observed difference between the flow behaviors of the two valve types is consistent with the difference in their performances. The backchannel diode tended to produce better structured jet earlier in the cycle than the open cusped valve. This could be explained by the unseen flow within the orifice of the valve. The flow separates from the end of the nozzle contraction of the open cusped diode and the jet begins to diffuse. This point is 2 - 3 mm upstream of the where the end of the annular ring that encloses the backchannel on the other design.

Thus, the flow field captured with PIV for the open cusped is of a more developed jet stream.

Shear Stress Level and Exposure Time

Analysis

Various studies suggest that the effect of shear stress on a platelet or erythrocyte is dependent not only on the magnitude of hat stress, but the amount of time that it is exposed to this level of stress. The PIV results for both the backchannel and the open cusped diode valve reveal that the highest levels of the turbulent shear stress occur at peak systole for the case with the highest PVR. The maximum values were measured in the area of the shear layer that formed between the jet flow exiting the valve and the lower wall of the main pulmonary artery.

The total shear was estimated as the sum of the viscous shear stress and the turbulent shear stress given in equation 19.

$$\tau_{total} = \tau_{xy} + \tau'_{xy} = \mu\left(\frac{d\bar{u}}{dy} + \frac{d\bar{v}}{dx}\right) - \overline{\rho u'v'} \qquad (19)$$

The term $\overline{\rho u'v'}$ most often has the opposite sign of the viscous shear in the same field; thus, the time average is expected to carry the same sign. Therefore, the total shear is the difference between the viscous shear and the turbulent shear stresses.

The level of activation as defined by Bluestein et al [55] was found using equation 20.

$$\text{Level of activation} = \sum(\bar{\tau}_{total} \cdot \Delta t) \qquad\qquad (20)$$

This level of activation method was calculated in the current study as a means to estimate the cumulative shear on a particle as it exits a diode valve and travels down the pulmonary artery.

The highest observed Reynolds shear stress was at the PVR = 6 mmHg/Lpm case for the backchannel diode during peak systole (t = 350ms). This flow and shear stress fields are shown in Figure 7.68 and Figure 7.69. The total shear stress for this case is also the highest. Figure 7.74 shows this the total shear stresses field and three streamlines within the flow field. The three streamlines were selected as representative of particle paths that experience high exposure to shear. The first path (identified as 1) originates at the valve exit and travels along the upper edge of the central core jet, to the downstream of the MPA and into the RPA near the distal wall. The second streamline (2) begins at the valve exit and flows downstream into the LPA. This streamline encounters the region that contains the peak RSS values. The final streamline (3) originates at the valve exit and travels along the edge of the shear layer in the lower MPA and LPA. This path also crosses areas with elevated viscous and turbulent shear stresses.

Since pulsatile flow was measured, and data was obtained in time intervals, some concessions were made in order to estimate the exposure time of a particle. In this case, the time interval at which data was collected was 50 ms. Therefore, the data collected at

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350 ms after the start of systole was assumed to be an average representation of the flow

data from t = 325 ms to t = 375 ms.
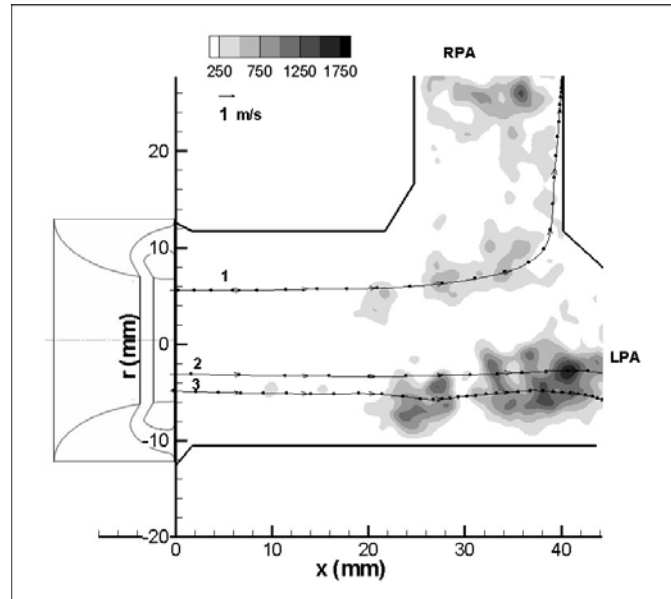
Figure 7.74. Total shear stress field and three streamlines for backchannel
diode at PVR = 6.85 mmHg/Lpm 350 ms after the start of systole.

Results

The markers on the streamlines indicated a particle moving in 1 ms time steps.

The particle along streamlines 1 and 3 are in the flow field for more than 50 ms.

Therefore, the cumulative shear stresses were calculated based on the 50 points that gave

the highest result. The particle in the second path flowed through the field of view in less

than 50 ms since its velocities were of higher magnitudes.

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Table 7.5 lists the shear stress exposure and average total shear stress for each pathway for the time period 325 ms to 375 ms for the backchannel diode valves at all PVR levels. The uncertainty in the level of activation and total shear stress Generally, the level of activation increases as the PVR increases. The average total shear stress also increases. At PVR = 3.2 mmHg/Lpm, the particle path along the third streamline along the lower edge of the jet ends up in a vortex. This resulted in the higher level of activation and average total shear stress.

Table 7.5. The level of activation and average total shear for 3 streamlines for the backchannel diode at all PVR (mmHg/Lpm) levels.

Streamline	$\sum(\bar{\tau}_{total} \cdot \Delta t)$ (dynes-s/cm^2)/ Average Total Shear (dynes/cm^2)			
	PVR = 3.2	PVR = 4.3	PVR = 5.1	PVR = 6.9
1	5.41 / 108	4.45 / 91	9.56 / 203	8.59 / 172
2	8.22 / 191	19.5 / 389	32.1 / 643	15.6 / 502
3	23.4 / 469	14.0 / 280	32.9 / 659	38.0 / 760

The first streamline had a level of activation of 8.59 dynes-s/cm^2. This streamline travelled along the existing shear layer between the jet and the area of recirculation and through a region of elevated turbulent shear near the RPA entrance. The level was lower than the equivalent 35 dynes-s/cm^2 that Ramstack et al. [54] found as the threshold for platelet activation. The average total shear for this pathway was 172 dynes/cm^2.

The second streamline that passed through the area of peak total shear stress located about 40 mm downstream of the valve exit. The level of activation was 15.6

dynes-s/cm^2. This path was also subjected to the highest velocities; thus, the particle displayed through the field in only 31 milliseconds. While this is higher than the streamline 1 level, it is still less than the threshold for platelet activation. The average shear stress on this particle was 502 dynes/cm^2.

The last streamline began at exit of the valve along the line of flow separation. This path flows the length of the MPA and into the LPA similar to the second streamline. The velocity of the particle on this path, however, is lower than that of the second streamline. As a result, the particle needed 75 ms to travel through the field. Therefore, the level of activation was based on the 20 - 49th points along the streamline. It was calculated to be 38.0 dynes-s/cm^2. This does pass the threshold established by Ramstack et al [54], thus, suggesting that at this PVR platelet activation may occur for this case.

<div align="center">LDV Results</div>

The laser Doppler velocimetry data was used to collect flow measurements on a backchannel flow diode. These measurements were made in accompaniment with the particle image velocimetry measurements. PIV was used to observe the behavior in the entire flow field. The PIV data was also used to calculate Reynolds shear and normal stresses. The LDV methods allow for a higher temporal resolution so that frequency analysis could be performed.

Testing

Data was only collected along the central, vertical plane of the flow field. The set up to gather data in the offset planes did not yield sufficient signal to noise ratio. The data points are shown in the grid in Figure 7.75. At every point in the grid 12,000 data points were collected at 1000 Hz.

The blood analog was a sodium iodide/glycerin water solution that had a similar refractive index as the acrylic test section. The flow was seeded with 2μm silicon carbide particles with a specific gravity of 1.6. This SG is also on the order of that of the blood analog.

The mock circulatory system was tuned to model physiological flow and pressure curves. The regurgitant fraction (RF) was 5% and the pulmonary vascular resistance (PVR) was 3 mmHg/Lpm.
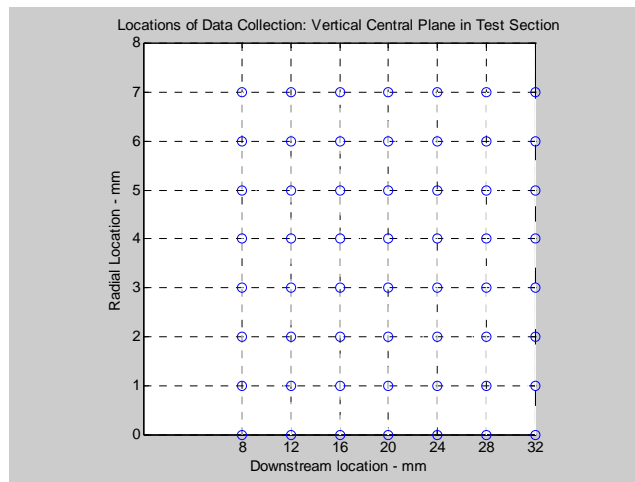
Figure 7.75. Positioning Grid of Data Points

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Post Processing

An algorithm written for Matlab® was used to post process the data. The data taken at every locale in the grid was saved as a different file containing the 12,000 data points. The signal was pulsatile, and was therefore made up of many cycles. The mock circulatory system was pumping at an approximated rate of 75 bpm, or 0.8 Hz. Therefore, there are up to 15 different cycles taken at every point.

The higher levels of turbulence stress were shown to take place within the shear layer created by the entrained jet in the PIV results. This was located in the outer 4-5 mm away from the centerline. The spectral analyses for select points are presented in Figure 7.76 and Figure 7.77.

. The first spectrum for the axial velocity component for a point 28 mm downstream of the valve and 6 mm above the centerline. Figure 7.76 shows that at the spectrum of the u'v', u'^2, and v'^2. The u'v' decays at a slope of -1, indicating that large scale turbulence existed. Above 100 Hz, the slopes drops to -5/3 suggesting that the flow was beginning to transition from large scale vorticity production to smaller scale eddies. The u' and v' components decay at a slope of -1.

The spectra analysis from further down in the stream (Figure 7.77) shows similar results. The u'v' term decays at -1 slope for approximately one decade. At frequencies above 200 Hz, the slope decreases to -5/3. The u'^2 has a similar trend as the -5/3 slope develops at higher frequencies.

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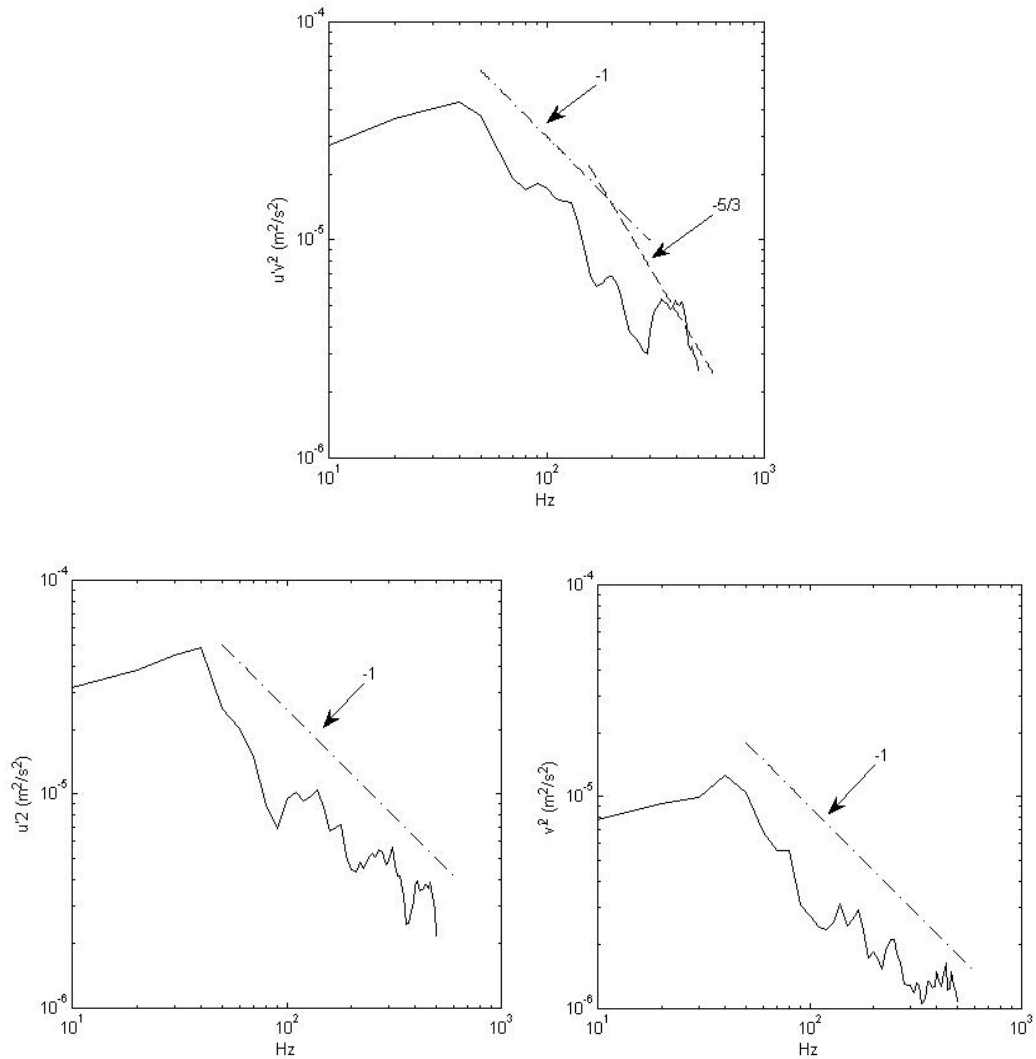
Figure 7.76. Spectrum 28 mm Downstream of Backchannel Diode Valve, 6mm above centerline
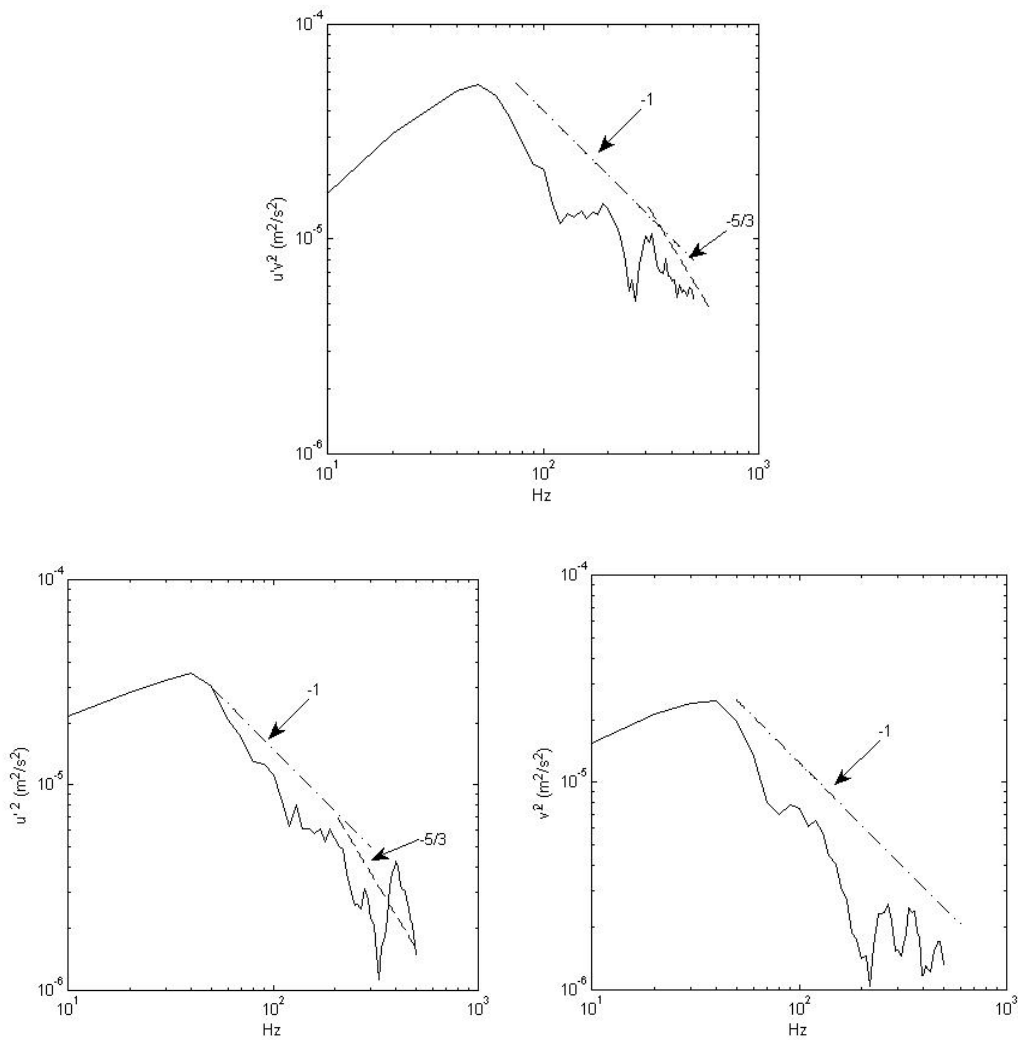
Figure 7.77. Spectrum 32 mm Downstream of Backchannel Diode Valve, 6 mm above centerline

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CHAPTER EIGHT

SUMMARY AND CONCLUSIONS

<u>Summary of Results</u>

Three objectives were posed in this study so as to evaluate momentum diode valves as pulmonary heart valve replacements. The first objective was to test the momentum diode valves *in vitro* over a range of physiological conditions and find the resulting transvalvular pressure gradients and regurgitant fractions. This was accomplished with the development of the mock circulatory system that allowed for testing over a range of physiological conditions. This method was used to then compare the abilities of the fluid diode valve to regulate flow to that of traditional replacement valves, such as bileaflet valve and a monoleaflet tilting disk.

In preliminary *in vitro* studies, the diode valve showed promise as both regurgitant flow and transvalvular pressure gradients were held to moderate levels for a range of pulmonary vascular resistances. The diode valve showed improvement in ability over the flow nozzle to impede regurgitant flow. For a PVR range of 1 to 5 mmHg/lpm, the diode valve yielded a RF% of 2% to 17% as compared to the 2% to 23% for the nozzle. Both valves had TVG values up to 17 mmHg. Though these were higher than the bileaflet and tilting disk valves, RF% and TVG were still within the acceptable range. Thus, the results of this study support the idea that a motionless momentum diode valve can be used to regulate flow in the pulmonary position.

The acute animal model showed no catastrophic effects of using a motionless pulmonary valve. An implantation strategy was developed that can be carried into a chronic test animal model. The i*n vivo* performance results were consistent in both tendency and magnitude with *in vitro* findings. In both cases, the RF% and TVG for normal values of PVC (2 to 3 mL/mmHg) and PVR (2.3 to 3 mmHg/Lpm were within levels known to be well tolerated in humans. Thus, these findings also suggest that the diode valve concept can be implemented as a pulmonary heart valve. However, a compromising factor in these tests was a valve size to patient mismatch, which likely altered valve flow into the pulmonary artery.

Another objective was to determine the influential geometric parameters on the valves performance. Each valve design maintained the transvalvular pressure gradient below 30 mmHg resistance up to 5 mmHg/Lpm. The RF% for all valves was less than 35% for PVR values below 4.5 mmHg/Lpm. At PVR = 2.5 mmHg/Lpm, some designs had RF% within the 0-20% range. The 60˚ backchannel diode had the lowest RF% and TVG for some levels of the resistance among the backchannel valves. Conversely, the 60˚ open cusped valve had markedly higher RF% and TVG measurements versus the other two valves. Therefore, results of this study further lent strength to the hypothesis that diode valves as replacement pulmonary valves. This study also identified the beta ratio and interaction between cusp type and the angle of impingement were as tow of the key parameters affecting the RF% for the diode valves. This information can be used to conduct further design optimization on the diode valves.

A final goal of this study was to use particle image velocimetry (PIV) to study the hemodynamic performance of different diode designs. The flow fields of both diode valves showed a jet entrained by areas of recirculation emerging from the valve orifice. At the highest PVR, the peak velocity through the pulmonary valve in this study were at times measured to be 2.5 times higher than 0.9 m/s, the average peak velocity in children [2]. During diastole, the flow was uniformly distributed. The flow speeds for the high resistance cases peaked at -0.93 m/s. There were slight differences in the flow fields between the valve types. The backchannel diode featured a better structured jet earlier in the cycle than the open cusped valve. This could be explained by the unseen flow within the orifice of the valve.

The PIV studies were conducted in part to determine if the momentum diode valve would cause shear stresses in the flow to be damaging to the red blood cells or platelets. The viscous and turbulent shear stresses were always highest during peak systole. The maximum viscous shear stress values were along the shear layer created by the jet. For all valves in all cases, the peak viscous shear stresses ranged from 30 and 64 dynes/cm^2. The highest turbulent shear stresses were located at the end of a region of recirculating flow leading into the left pulmonary artery. There were also elevated shear stresses near the RPA and MPA branch. The highest RSS is 1720 dynes/cm^2. The highest measured shear stress was acquired for the backchannel diode at the highest PVR during peak systole. The maximum total shear stress was also observed for this case. The peak level of activation for a particle travelling in the field was found to be 38 dynes-

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s/cm^2. This was 10% higher than the threshold (35 dynes-s/cm^2) reported to trigger platelet activation.

Raised wall shear stress levels were also of concern in this study since they can result in platelet activation and can trigger eNOS. The distal wall of the RPA was subjected to highest wall shear stresses at times. At peak systole, the flow into the RPA was skewed toward the distal wall resulting in shear stresses as high as 30 dynes/cm^2. This was less than the 91 dynes/cm^2 reported to cause platelet activation, yet higher than the 25 dynes/cm^2 stated to elevate eNOS.

The regions of recirculation present during peak systole and mid diastole periods, leaving possibilities for platelet aggregation to take place. The diastolic flow was uniformly distributed and was shown to sweep the MPA walls with shear stresses between 3-10 dynes/cm^2. This is a good range for wall shear as it is high enough to effectively wash the walls, but not so high as to trigger platelet activation or release of the eNOS synthase.

The results from particle image velocimetry revealed that the in many cases, for levels of regurgitation less than 20%, the flow through the diode valves would not be expected to have problems with platelet damage, RBC damage or platelet aggregation. However, in the case with the highest levels of total shear stress, the level of activation threshold was exceeded and wall shear along the RPA wall was high enough to trigger

the release of a vasodilator. So, the diode valve is a plausible solution under certain physiological conditions.

Conclusions

There are many conclusions that can be taken away from this study. The results of this study support the original hypothesis with some caveats. First, an experimental system was developed that was capable of generating physiologically accurate pressure and flow signals for the pulmonary circulation.

This system was then used to test the conceptual fluid diode in the pulmonary position and the results of the *in vitro* tests showed that a fluid diode valve could acceptably regulate flow the mild levels tolerable in the pulmonary circulation.

The acute *in vivo* study also showed that the diode valve has promise as a pulmonary heart valve replacement. The implanted diode was able to regulate flow under a range of physiological conditions. Moreover, information was gathered on how to proceed with further animal studies. This information included the preferred surgical techniques, the need for special implantation tools for the diode valves, the size and layout of the swine's heart and pulmonary artery.

The parametric study identified the beta ratio dimension as having a large effect on the performance of the fluid diode. The cusp enclosure design and the angle of impingement had varying effects and suggested an interaction of the two dimensions. This information can be used to further optimize the diode design.

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Finally, the outcome of the hemodynamic study further supported the hypothesis. The level of activation was shown to be a function of the pulmonary vascular resistance and it did not exceed the threshold until the highest level of PVR.

Recommendations

Based on the knowledge of testing methods, diode design and the results from this the present work, the author has a few recommendation for future work. First, there are a few suggested changes to the MCS. A ventricle design in which the pressure-volume curve can be controlled and varied to better simulate the function of the heart should be implemented. Also the updated ventricle should also be capable of higher heart rates and stroke volumes so that a wider range of physiological conditions, such as exercise, can be simulated. The effect of the ventricular – arterial coupling should be studied as it

Since the ability to control the PVR affected the outcome of the parametric testing, future tests should be carried out using CFD and/or other computational modeling techniques. The factors will be better controlled; thus, the tests will be able to more accurately predict the effects of changing geometries.

There are many potential flow studies that can be carried out. The differences between the backchannel and open cusped diode valves should be studied experimentally using diodes made of acrylic or other material that will permit for optical studies. In this way, the flow detail within in the flow channel and cusps of the valves can be seen. Scaling tests should be conducted in order to find out how smaller diodes compare to the

25 mm diodes tested in the current study. Also, the long term effects of the low wall shear that occurs in the pulmonary artery as a result of the entrained jet should be explored in order to understand what effect this may have on the vessel walls.

The outcome of the animal model should be taken and applied to future in vivo tests. The importance of the valve size was emphasized in the animal study. The test protocol should be expanded to include a better control test. It was shown that an animal with a healthy heart may not be able to handle the shock of the mild regurgitation and pressure gradients that are associated with the fluid diode valve. Therefore, an approach should be developed that takes this into account.

APPENDICES

Appendix A

Multi-Scale Model of the Fluid Diode in the Mock Circulatory System

The lumped parameter model of the mock circulatory system was developed by Dr. Tim Conover. This appendix contains an excerpt of a report by Conover [122] that describes the LPM.

Modeling the MCS

Figure A.1 shows the network model to simulate the upstream portion of the MCS in terms of lumped parameter (zero-dimensional) elements. The source of the blood analogue fluid is a constant head tank set to provide the systemic venous pressure P_{SV}. A "big" hose connects the constant head tank to a ball check valve, which simulates the tricuspid valve of the heart (the action of the right atrium is generally considered negligible with respect to the pulmonary valve, our area of interest). The model of the big hose includes quadratic resistance (for both viscous flow and turbulent flow with Darcy friction factor f=0.02), an exit loss into the constant head tank during reverse flow only, and inertance. Flow through the big hose is equal to flow through the tricuspid check valve, Q_{TC}.

The ball check valve has a certain range of travel, giving it three effective states, and it requires a certain amount of reverse flow to close it. In reverse flow, the moment the ball is seated, shutting the valve, Q_{TC} is decelerated to zero impulsively. This is the closed state. When downstream pressure falls below upstream pressure, the ball opens and Q_{TC} accelerates. In the free state, the ball is assumed to have neutral buoyancy, so it

travels with the fluid, and it adds no resistance to the flow. The ball's position is represented by the volume of fluid that sweeps it along, V_{BV}, which is the time-integral of Q_{TC}. The ball strikes a pin limiting its forward travel, setting the pinned state. The minimum value of V_{BV} to strike the pin, according to the geometry of the ball valve chamber, is 10.2 ml. In the pinned state the fluid must accelerate through the annular gap between the ball and the cylindrical walls of its chamber, causing a pressure drop in the manner of an orifice. When Q_{TC} reverses the ball moves freely again, backwards, until it closes.
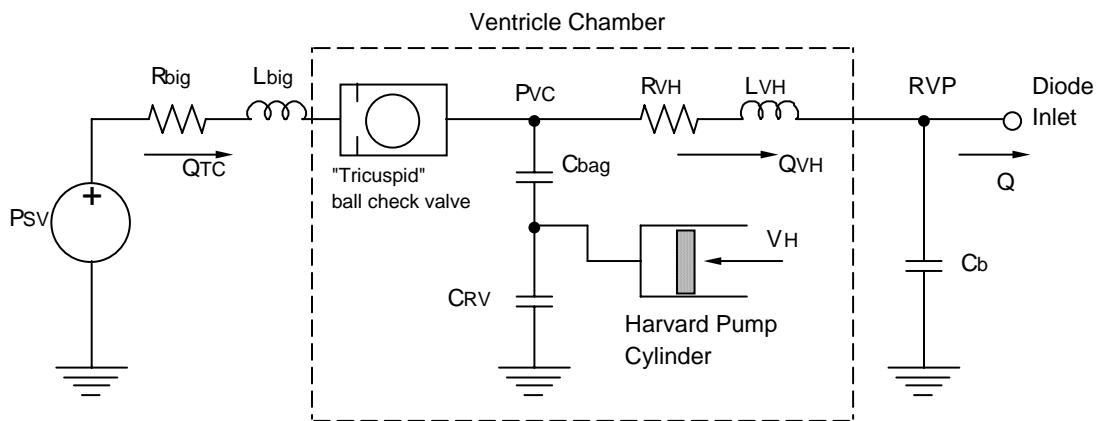
Figure A.1. Lumped parameter model for the upstream of the Mock Circulatory System.

Flow through the ball valve enters the ventricle chamber, in which the flow is confined in a concentric respirator bag, similar to the construction of the pulmonary compliance chambers. Both the elasticity of the bag and the compressibility of air

trapped in the chamber contribute to the pressure on the fluid, P_{VC}. In Figure A.1 these two mechanisms are indicated by the compliances C_{bag} and C_{RV} in series. C_{RV} can be estimated from the volume of trapped air, but C_{bag} is not well-known, and it is generally nonlinear. Fortunately C_{bag} is relatively large, so the effect on P_{VC} is relatively weak. To produce pulsatile flow, the cylinder of the Harvard Pump is used to cyclically displace an additional volume of fluid V_H into the space outside the bag. The stroke rate and systolic ratio are settings on this pump that are also confirmed through data acquisition, systole being indicated by a microswitch installed on the crankshaft. The stroke volume is measured manually. Because C_{bag} is unknown and nonlinear, it is ignored in the lumped parameter model, effectively short-circuiting it in Figure A.1. C_{RV} is reduced somewhat to approximate the lost compliance. Experience has shown that the overall performance of the lumped parameter system is not very sensitive to minor variations of C_{RV}.
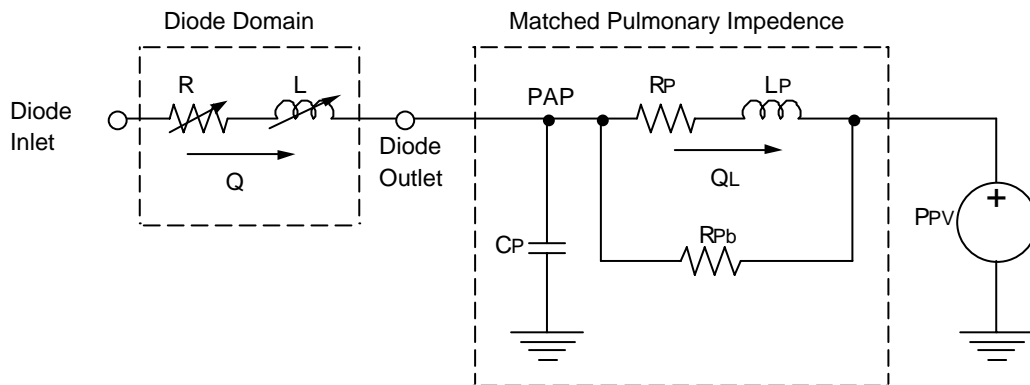
Figure A.2. Lumped parameter model for the fluid diode, and the downstream pulmonary impedance.

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The flow out of the ventricle chamber and through the hose to the test section is Q_{VH}. The hose is modeled with a quadratic resistance (with the turbulent friction increased to f=0.06 to accommodate the several barbs in this hose), an exit loss into the test section during forward flow only, and an inertance. Finally, Figure A.1 shows a buffer compliance element with compliance C_b, operating at the Right Ventricular Pressure (RVP). This small-value compliance does not represent any perceptible compliance in the real test section, but it is necessary to stabilize the numerical model. The RVP sets the inlet boundary of the model in Fluent, and it represents the RVP which is measured in the real test section.

Figure A.1 shows the lumped parameter model of the "diode," which is actually the whole test section, and the pulmonary impedance. The flow rate through the diode is Q. The pressure-flow characteristics of the fluid diode can be approximated by a nonlinear quadratic resistance and a nonlinear inertance in series, a total of six parameters. This model is accurate enough for design of experiment work, and for setting up initial conditions for the multi-scale model in Fluent. Naturally the six-parameter model is not part of the model in Fluent.

There was a considerable effort made to model the actual physics of the downstream section of the MCS in terms of lumped parameters. Unfortunately the concentric compliance chambers are complex, nonlinear, continuous systems, and the modeling results were not good. Alternatively, for a given experimental case, a linear systems technique can be used to identify a non-unique system of linear components

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matching the pulmonary impedance which was observed in that case. Unfortunately this matched system for one case is not generally applicable to other cases, but it is sufficient to provide a downstream boundary condition in Fluent to simulate that case.

Therefore, Figure A.2 shows, not a representation of the downstream part of the MCS, but a simple system of linear components which can be tuned to match both the DC resistance and the impedance at the fundamental frequency, which was calculated from a given experimental data set. First there is a pulmonary compliance element with compliance C_P, operating at the pulmonary artery pressure PAP. The PAP sets the outlet boundary in Fluent, and it represents the PAP measured in the real test section. Next the flow divides into two parallel branches. One portion of the flow, Q_L, passes through the inertial branch, having both resistances R_P and inertance L_P. The remainder of the flow passes through the bypass branch, having only resistance R_{Pb}. Both branches drain into the "pulmonary veins" constant-head tank, which sets the final pressure P_{PV}, and is the same as the corresponding tank in the actual MCS. In the Laplace domain, the input impedance spectrum of this system is

$$Z(s) = \frac{sR_{Pb}L_P + R_P R_{Pb}}{s^2 R_{Pb}L_P C_P + s(R_P R_{Pb}C_P + L_P) + R_P + R_{Pb}}. \qquad \text{(A.1)}$$

Results from Lumped Parameter Model Tests

Table A.1 shows all the results from the LPM using different upstream inertance values. The inertance level for the system as it was originally calibrated was 8.79E-3 mmHg-s^2/mL. When the inertance was 3.4E-2 mmHg-s^2/mL, there was minimal backflow.

Table A.1. Results from LPM Tests

Lvh (mmHg-s^2/mL)	CO (Lpm)	RF %	PVR (mmHg/Lpm)	PVC (mL/mmHg)	TVG (mmHg)
8.79E-03	5.3	11.1	3.1	2.9	6.9
4.00E-03	5.1	11.7	3.2	2.7	7.9
2.00E-03	5.1	11.8	3.2	2.7	8.1
1.00E-03	5.1	11.7	3.2	2.7	8.6
1.50E-02	5.7	8.6	3.0	3.2	6.5
3.00E-02	7.5	1.09	2.6	4.0	9.5
3.40E-02	7.8	0.08	2.6	4.3	9.7
6.00E-02	9.9	0.0	2.3	6.5	11.4

Open Cusped Diode - Case 2

The pressure and flow curve for the moderate PVR and RF% case is shown in Figure B.1. The flow rates range from 14 Lpm to – 3.5 Lpm. The PVR = 4.3 mmHg/Lpm. The regurgitant fraction for this setting is 12.4%.

Early systole (t = 150 ms)

Figure B.2 shows the flow and viscous shear stress fields at the PVR = 4.3 mmHg/Lpm case 150 ms into the cycle. The average velocity in the MPA at this time in the cycle is -0.0333 m/s. the peak velocity is – 0.17 m/s. Noticeable reverse flow from the LPA reenters the MPA and an area of recirculation is formed in the lower radial part of the main artery. Also, the flow from the RPA rejoins the flow in the MPA and impinges upon the retrograde jet from the LPA. On the upper main artery wall, there is another region of recirculation between the regions of retrograde flow and antegrade flow.

The measured viscous stresses are very low; they are less than 6 dynes/cm^2. The highest bulk flow stresses at this point occur along the shear layer resulting from the flow from the LPA and RPAs mixing shown in Figure B.2.

The peak turbulent shear stresses during early systole are on the order of 50 dynes/cm^2 (Figure B.3). This coincides with region where the branch flows collide and

where the shear layers exist (Figure B.2). The peak turbulent stresses 150 ms for the Case 2 are 2 – 3 times higher than Case 1 (PVR = 3.1 mmHg/Lpm) likely because of a higher rate of mixing there.

Peak Systole (t = 350 ms)

At peak systole, a central jet structure is discernible (Figure B.4). There is an area of recirculation along the lower radii of the MPA, that reattaches before the entering the LPA. Moreover, unlike the PVR = 3.1 mmHg/Lpm case, there is no recirculation in the RPA branch. Instead, the flow follows the RPA bend well. Therefore, the secondary flow in both branches is well formed. The flow once again impinges the artery wall at the bifurcation. The peak velocities are 1.32 m/s and the average MPA velocity is now 0.504 m/s.

As the cycle progresses, and peak systole is reached (t = 350 ms) the peak viscous shear stresses are about 35 dynes/cm^2 (Figure B.4). They occur along the edges of the entrained jet structure. The magnitudes are similar to those observed in Case 1. The primary flow branches into the RPA rather smoothly and this results in well defined flow into RPA. Thus, there are measureable wall shear stresses along the distal RPA wall. Additionally, there is a shear layer present between the proximal RPA wall and the jet flow into the RPA.

Figure B.5 shows the Reynolds shears stresses field at t = 350 ms after the start of systole. The turbulence levels are less in this case than at PVR = 3.1 mmHg/Lpm.

(Figure 7.7). At the lowest PVR, the flow field had an area of recirculation that created mixing near the RPA and MPA and between the LPA and MPA. For PVR = 4.3 mmHg/Lpm, the flow transitions more smoothly into the RPA as shown in Figure B.4. One of the locations where peak turbulent shear stresses occur is in the 90º turn in the RPA where flow separation occurs. Also, RSS levels are 200-300 dynes/cm^2 along both walls of the main artery and at the inner RPA wall within the shear layer that exists.

Mid Diastole (t = 550 ms)

As the flow decelerates, the jet structure is still present (Figure B.6). There are noticeable shear layers between the regions of antegrade and retrograde flow in the upper and lower radial locations of the main pulmonary artery. At this point in the cycle an area of recirculation is now seen in the RPA entrance; thus, resulting in an area of stasis. The peak and average MPA velocities are 0.824 m/s and 0.286 m/s, respectively.

The peak shear stress values at 550 ms after the start of systole are about 14 dynes/cm^2 (Figure B.6). This is comparable to the 1st case. These areas of higher shear are along the edges of the jet structure, at the distal RPA wall, and between the antegrade flow and the lower MPA wall.

Figure B.7 show the turbulent shear stress field 550 ms after the start of systole for PVR = 4.3 mmHg/Lpm. The turbulent shear stresses are high at the edge of the combining flow of the RPA and MPA (Figure B.6). Also, some of the highest levels take

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place where the flow separation occurs in the LPA. This is similar to the PVR = 3.1 mmHg/Lpm case during mid diastole.

Late Diastole (t = 750 ms)

The diastolic flows plotted in Figure B.8: shows well defined, undisturbed retrograde flow in the MPA and the branches. There is a small area of stasis near the branch between the left and right branches. Otherwise, the flow is sufficient to promote wall shear stresses needed to wash the artery wall. The peak velocities are -0.413 m/s and the average velocity is similarly -0.149 m/s.

The peak shear stresses of 10 dynes/cm^2. These are along the lower MPA and LPA walls where the most noticeable retrograde flow existed. At the other walls the shear was one half of the peak.

The turbulent shear stresses during diastole are shown in Figure B.9. The values are less than 40 dynes/cm^2 everywhere except where the retrograde flows from the left and right arteries meet. The RSS values for PVR = 4.3 mmHg/Lpm are double of that for PVR = 3.1 mmHg/Lpm.
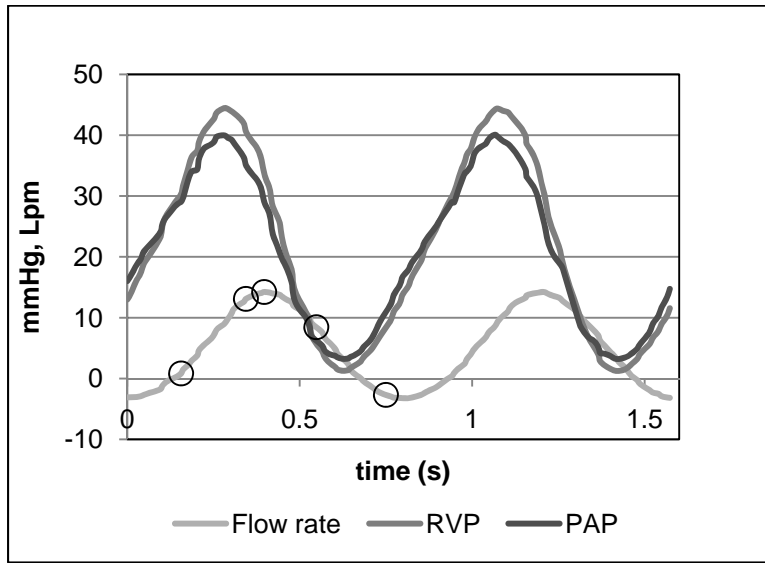
Figure B.1: Flow and pressure curves for the open cusped diode

Figure B.2: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after the start of systole for PVR = 4.3 mmHg/Lpm

Figure B.3: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 150 ms after the start of systole for PVR = 4.3 mmHg/Lpm, central plane

Figure B.4: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR = 4.3 mmHg/Lpm

Figure B.5: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 350 ms after the start of systole for PVR = 4.3 mmHg/Lpm, central plane

Figure B.6: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR = 4.3 mmHg/Lpm

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Figure B.7: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 550 ms after the start of systole for PVR = 4.3 mmHg/Lpm, central plane
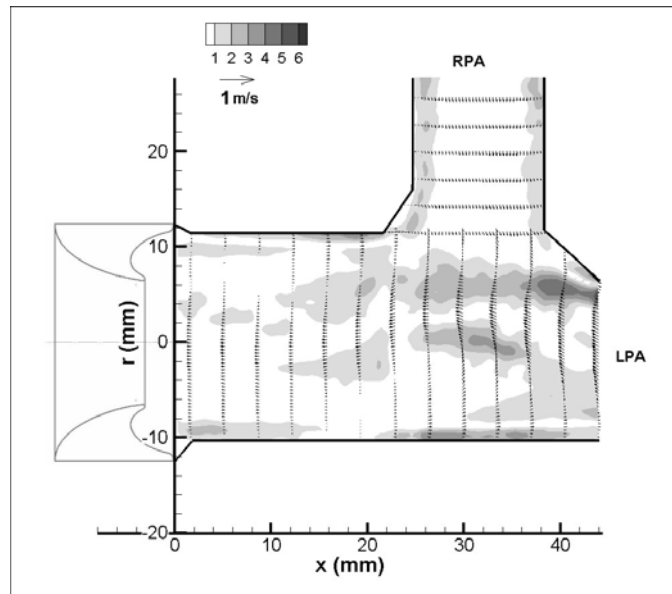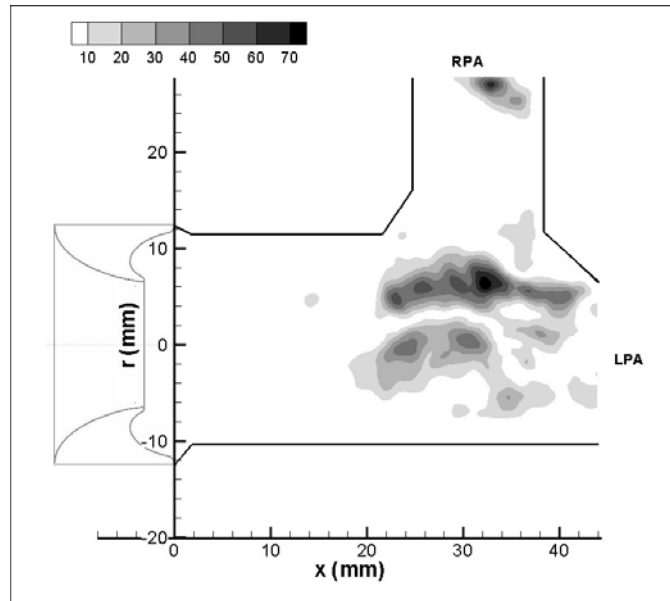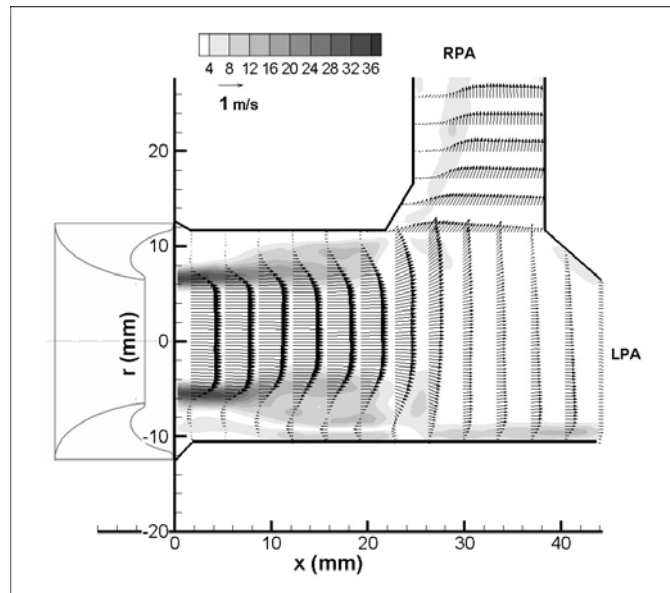

Figure B.8: Central plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR = 4.3 mmHg/Lpm

Open Cusped Diode Case 2 - Offset Planes

Figure B.10 shows the offset plane flow and viscous shear stress for the moderate PVR and RF% case at 150 ms after the start of systole. The flow profile is uniform. The average axial flow is -0.044 m/s, and the peak velocity is -0.170 m/s. The viscous shear stresses are highest near the walls. The peak value is between 3-4 dynes/cm^2. The Reynolds shear stress field is in Figure B.11. There is little disturbance in the MPA within 22 mm of the valve exit. The peak RSS values reach up to 25 dynes/cm^2.

At peak systole the velocity profile is parabolic (Figure B.12). A jet structure is evident just as it was in the central plane. The average axial velocity is 0.422 m/s. The peak velocity is 1.27 m/s. The bulk flow shear stresses are up to 25 dynes/cm^2 just as the jet forms at the valve exit. The wall shear stresses are up to 4 dynes/cm^2 where the flow has reattached to the artery wall. The offset plane Reynolds shear stresses at peak systole are shown in Figure B.13. The high regions are near the areas of recirculation 6 mm away from the centerline with maximum values of RSS up to 250 dynes/cm^2.

The offset plane flow and viscous shear stresses during deceleration at PVR = 4.25 Wood's unit are in Figure B.14. The peak axial velocity is 0.693 m/s. The average velocity is 0.207 m/s. The peak hydraulic shear stresses are 14 dynes/cm^2. The peak RSS values are on the order of 150 dynes/cm^2, lower than at peak systole (Figure B.15). The higher regions of turbulence shear stress take place in the areas of recirculation.

During diastolic flow in the offset plane is well organized retrograde flow (Figure B.16). The peak and average axial velocities are -0.270 m/s and -0.162 m/s, respectively. The flow, just as it was in the central plane, is uniform resulting in the wall stresses being the highest in the field. The peak shear stresses up to 9 dynes/cm^2. The turbulence levels decrease as the cycle reaches diastole (Figure B.17). The peak RSS values are around 40 dynes/cm^2. The highest values within the 22 mm of the valve exit occur at the most distal location, near the arterial branch.
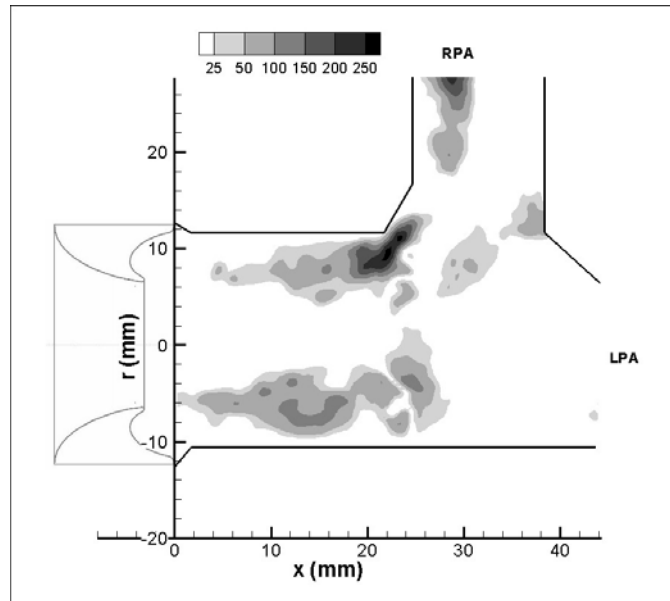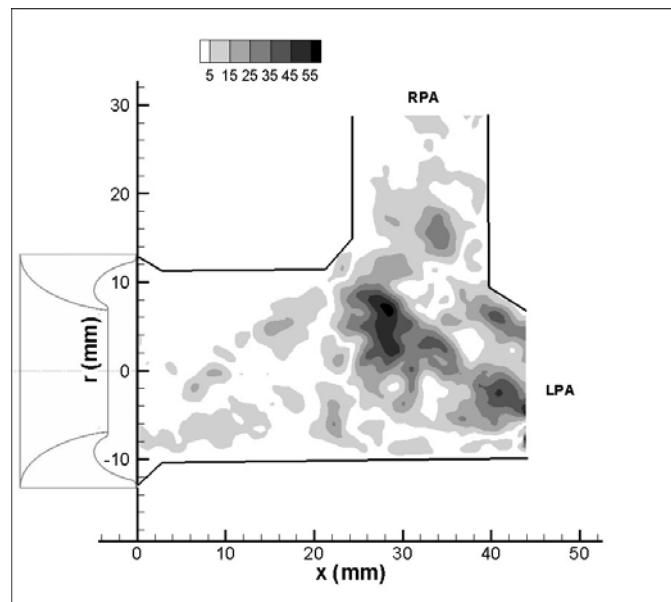

Figure B.9: Reynolds shear stress field (dynes/cm^2) for the open cusped diode at 750 ms after the start of systole for PVR = 4.3 mmHg/Lpm, central plane
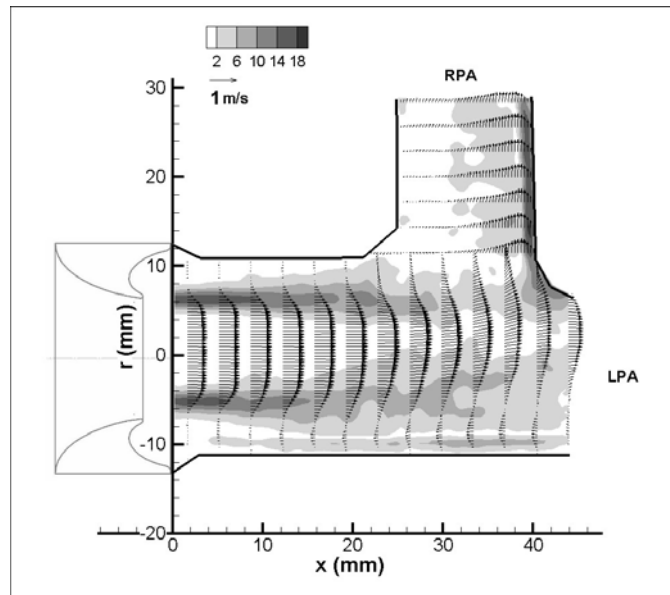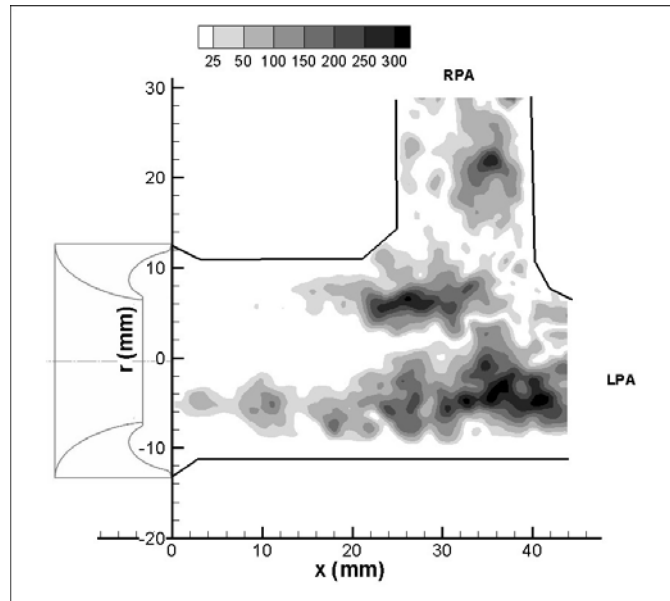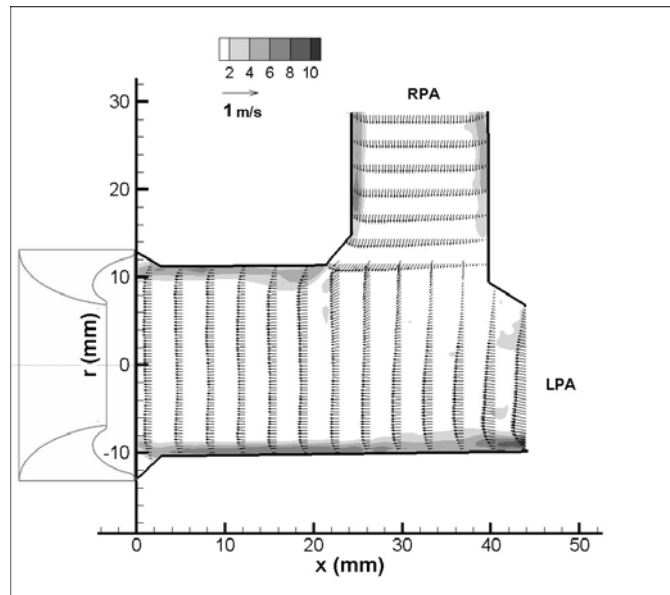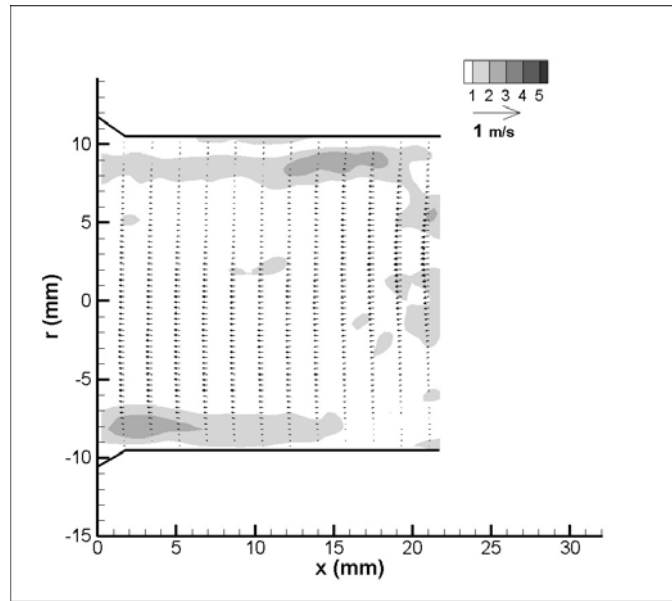
Figure B.10: Offset plane flow and viscous shear stress (dynes/cm^2) field at 150 ms after start of systole for the open cusp diode at PVR = 4.3 mmHg/Lpm
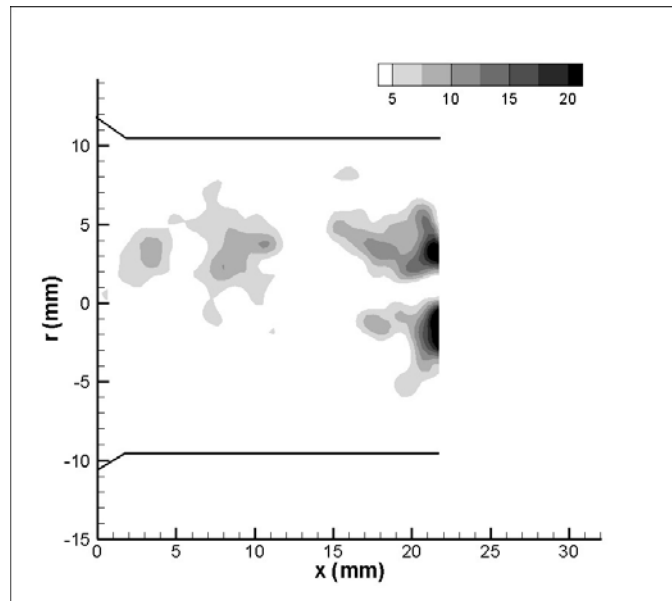
Figure B.11: Offset Reynolds shear stress (dynes/cm^2) field at 150 ms after start of systole for the open cusped diode at PVR = 4.3 mmHg/Lpm
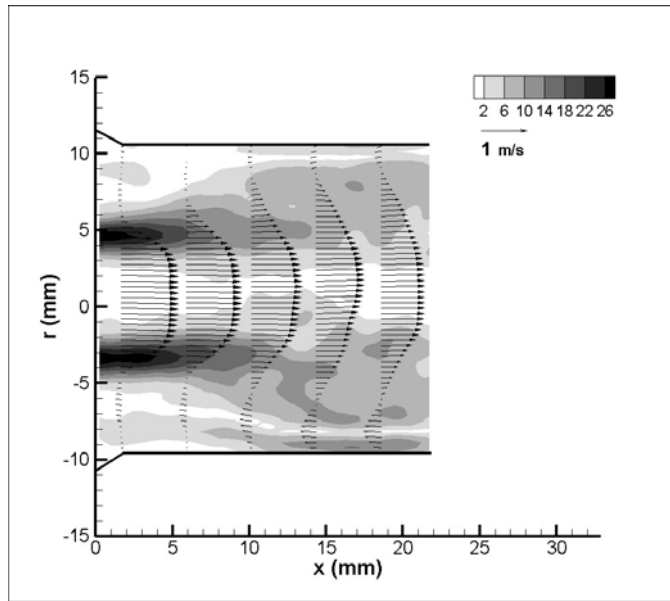
Figure B.12: Offset plane flow and viscous shear stress (dynes/cm^2) field at 350 ms after start of systole for the open cusp diode at PVR = 4.3 mmHg/Lpm
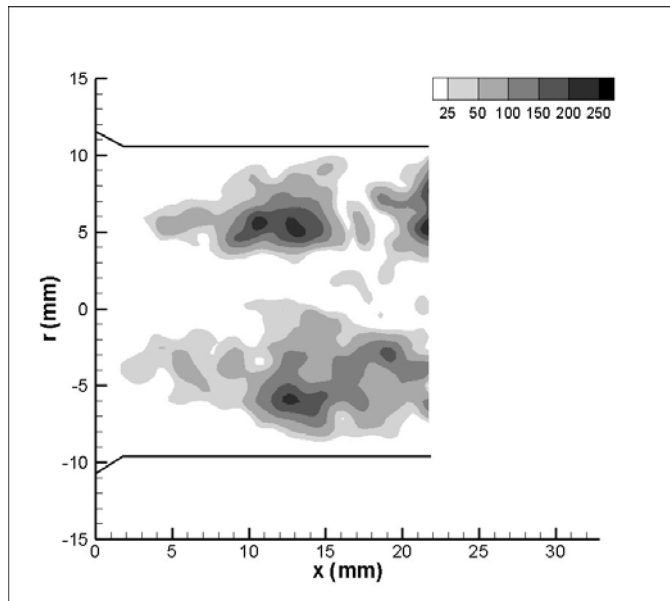
Figure B.13: Offset Reynolds shear stress (dynes/cm^2) field at 350 ms after start of systole for the open cusped diode at PVR = 4.3 mmHg/Lpm

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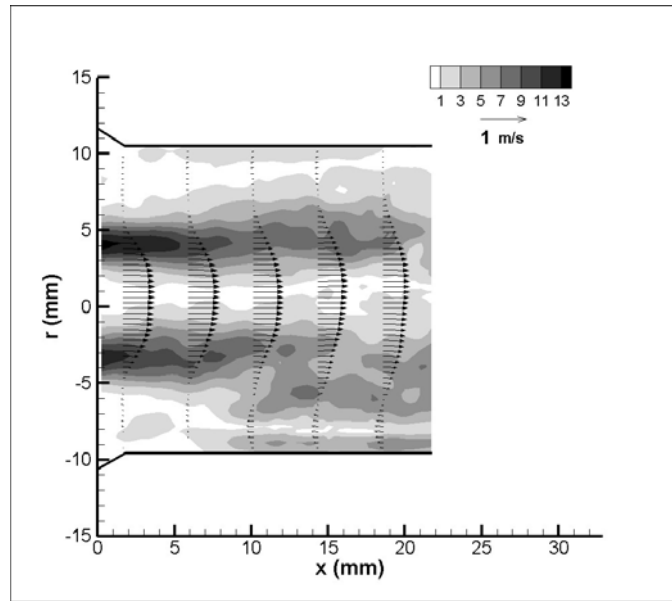
Figure B.14: Offset plane flow and viscous shear stress (dynes/cm^2) field at 550 ms after start of systole for the open cusp diode at PVR = 4.3 mmHg/Lpm
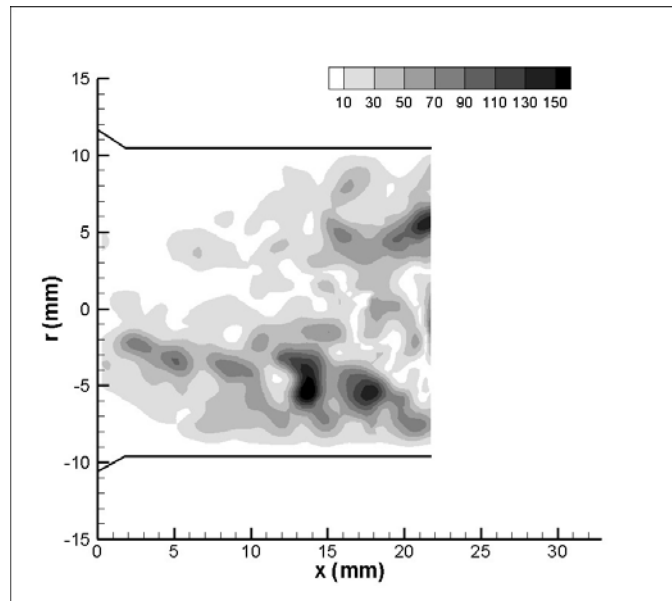
Figure B.15: Offset Reynolds shear stress (dynes/cm2) field at 550 ms after start of systole for the open cusped diode at PVR = 4.3 mmHg/Lpm
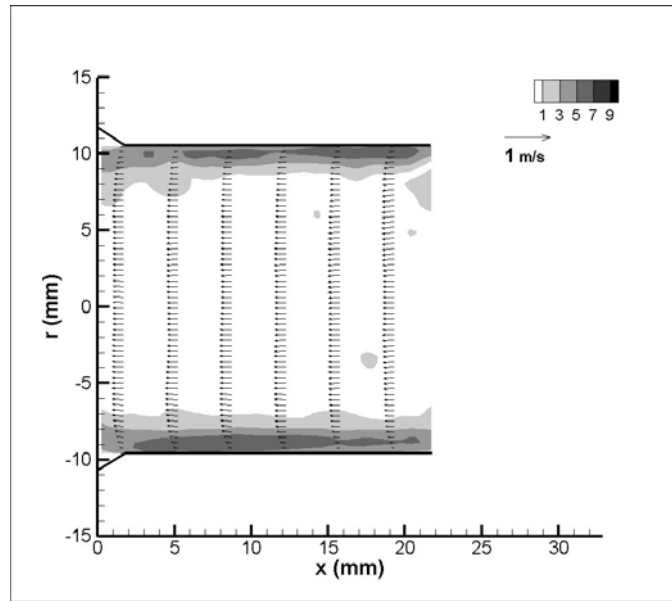
Figure B.16: Offset plane flow and viscous shear stress (dynes/cm^2) field at 750 ms after start of systole for the open cusp diode at PVR = 4.3 mmHg/Lpm
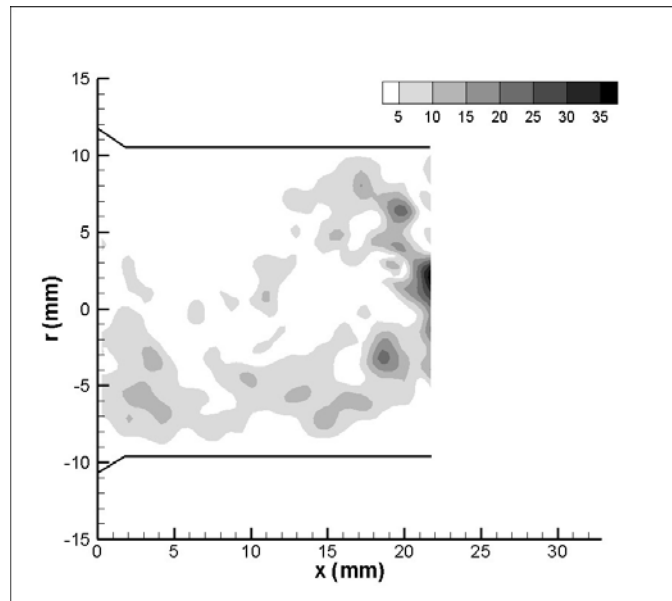
Figure B.17: Offset Reynolds shear stress (dynes/cm^2) field at 750 ms after start of systole for the open cusped diode at PVR = 4.3 mmHg/Lpm

Open Cusped Diode Case 3 – Offset Planes

Early Systole (t= 150 ms)

The velocity and viscous shear stress profile for the offset plane at t = 150 ms is shown in Figure B.18. The flow is uniform and diminishing at the walls. Therefore, the shear stresses are highest at the walls.   The peak viscous shear stress is less than 5 dynes/cm^2. The average velocity is -0.0056 m/s in the main pulmonary artery with peaks up to -0.202 m/s. Figure B.19 is the Reynolds shear stress field 150 ms after the start of the cardiac cycle. The turbulent stresses range up to 40 dynes/cm^2. The peak RSS occur on the centerline approximately 20 mm downstream.

Figure B.18: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after start of systole at PVR = 5.1 mmHg/Lpm

Figure B.19: Offset Reynolds shear stress (dynes/cm^2) field for the open
cusped diode at 150 ms after start at PVR = 5.1 mmHg/Lpm

Systole (t = 350 ms)

The offset plane flow and viscous shear stress field during systole shows a developing jet structure (Figure B.20). The areas of recirculation are seen 5 mm from the centerline. The flow reattaches to the wall in the lower MPA. The peak velocity is 1.64 m/s and averaged 0.463 m/s. The peak viscous shear stresses are along the edges of the jet. The highest shear values are seen just at the valve exit at 42 dynes/cm^2. The wall shear stresses are measured at 4 dynes/cm^2 at the upper MPA wall and 9 dynes/cm^2 at the lower wall. Figure B.21 shows the turbulent shear stress field at 350 ms after the start of systole. The highest RSS values are 42 dynes/cm^2.

Figure B.20: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after start of systole at PVR = 5.1 mmHg/Lpm

Figure B.21: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after start of systole at PVR = 5.1 mmHg/Lpm

Peak systole (t = 450 ms)

The peak flow rate occurs at 450 ms after the start of systole. The offset plane flow and shear stresses fields are shown in Figure B.22. The jet structure is well developed. The maximum axial velocity is lower than at 350 ms, at 1.60 m/s, and the average is 0.463 m/s. The peak viscous shear stresses along the edges of the jet are 35 dynes/cm^2. This is also lower than at 350 ms. The reverse flow is of a lower magnitude at the upper MPA than at the lower wall. Therefore, the wall shear stresses are less than 3 dynes/cm^2 at the upper wall and as high as 8 dynes/cm^2. The highest turbulent shear stresses at peak systole were observed in the areas of recirculation (Figure B.23). The RSS values peak at 350 dynes/cm^2.

Figure B.22: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 450 ms after start of systole at PVR = 5.1 mmHg/Lpm

Figure B.23: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 450 ms after start of systole at PVR = 5.1 mmHg/Lpm

Mid Diastole (t = 550 ms)

Figure B.24 shows the velocity profile during the mid diastole phase of the cycle. The velocities have lessened and the profile has flattened out. The average is 0.79 ms/ and the peak is 1.0 m/s. The shearing rate is also lower; the peak viscous shear stresses are only 13 dynes/cm^2. The wall shear stresses are less than 6 dynes/cm^2. The turbulent shear stress levels are similar to that observed at peak systole (Figure B.25). The field nearer the upper MPA wall has turbulence levels up to 235 dynes/cm^2 and the area in the lower radial position has RSS values as high as 350 dynes/cm^2.
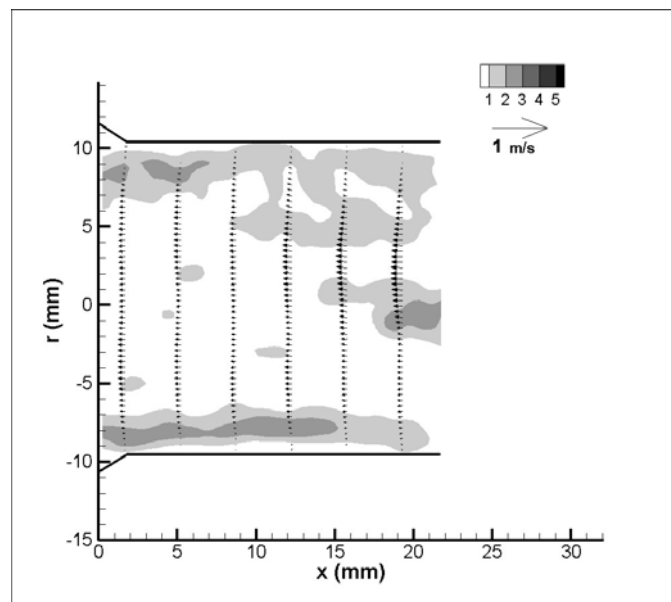
Figure B.24: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after start of systole at PVR = 5.1 mmHg/Lpm

Figure B.25: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after start of systole at PVR = 5.1 mmHg/Lpm

Strong retrograde flow is present during diastole as seen in Figure B.26. The flow is like that in the central plane. It is uniform. The peak velocity is 0.358 m/s and the average velocity is 0.214 m/s. The highest shear stresses are about 10 dynes/cm^2 and occur along the walls. At this point in the cycle, the Reynolds shear stresses measure less than 50 dynes/cm^2.

Figure B.26: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after start of systole at PVR = 5.1 mmHg/Lpm
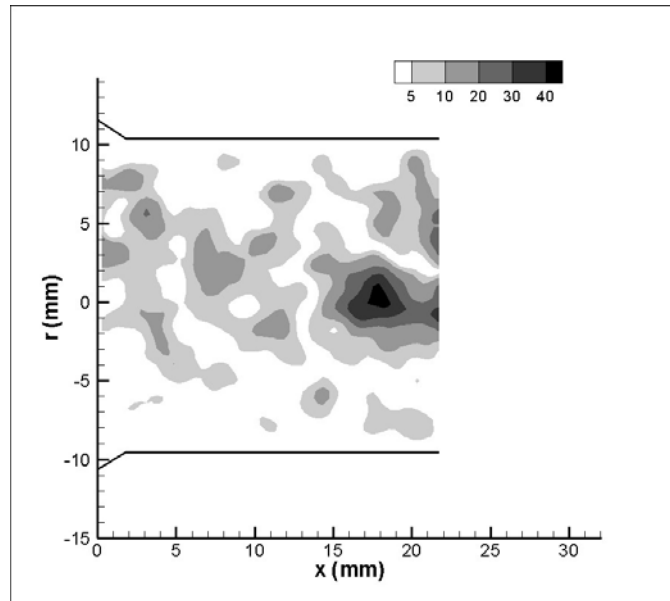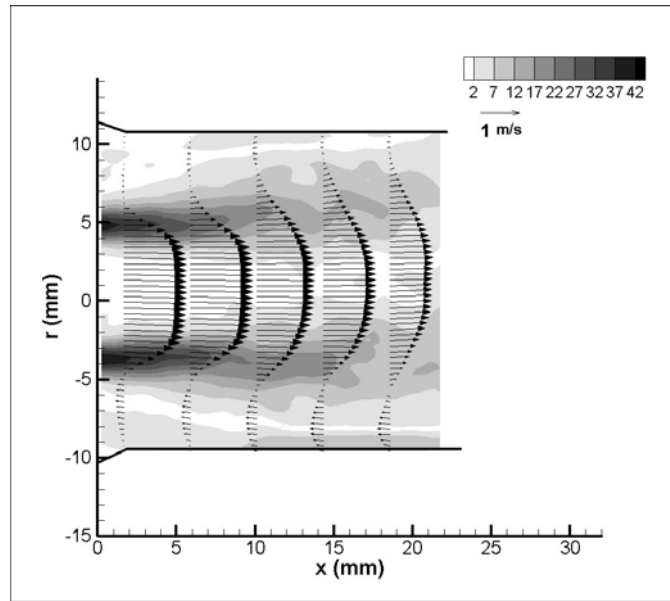
Figure B.27: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after start of systole at PVR = 5.1 mmHg/Lpm

Open Cusped Diode Case 4 – Offset Plane

Early Systole (t = 150 ms)

The offset flow plane for the open cusped diode is shown in Figure B.28. The flow field presented for this plane is only in the main pulmonary artery. The flow at 150 ms after systole start is uniformly distributed. The average axial velocity is 0.103 m/s. The peak velocity is 0.379 m/s. The peak shear stress is 8.7 dynes/cm^2. The Reynolds shear stresses within the first 22 mm of the valve exit are low, as the highest turbulence shear stress levels occur in the area of the artery branch (Figure B.29).

Figure B.28: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after the start of systole for PVR 6.1 mmHg/Lpm
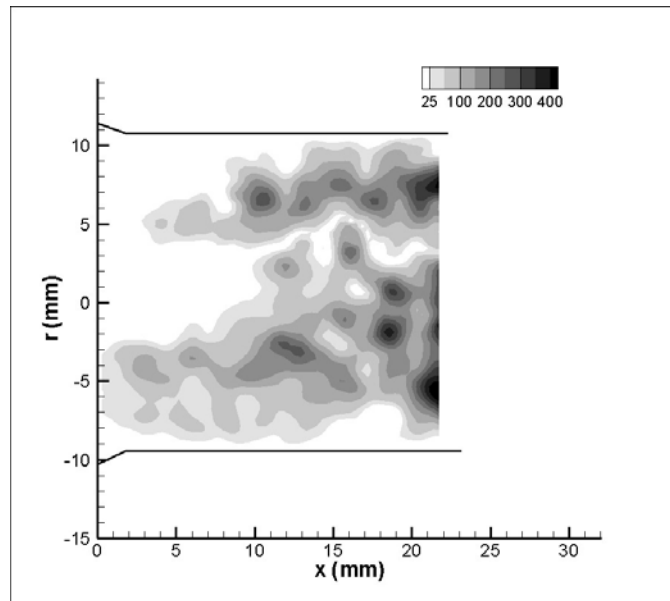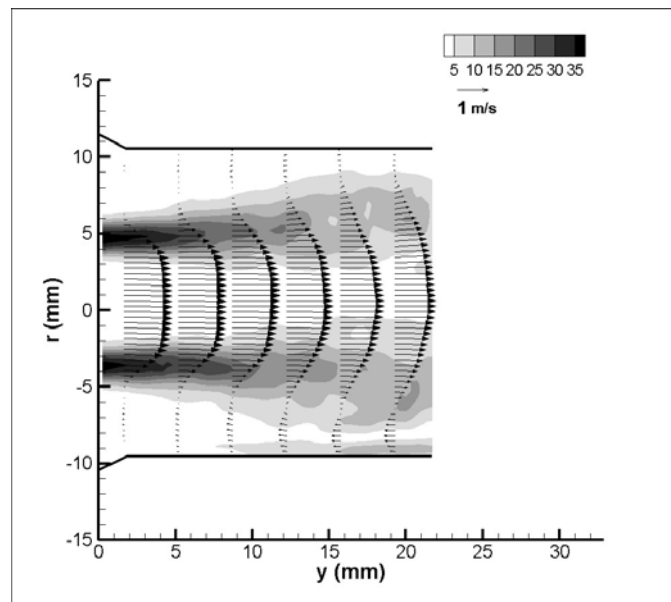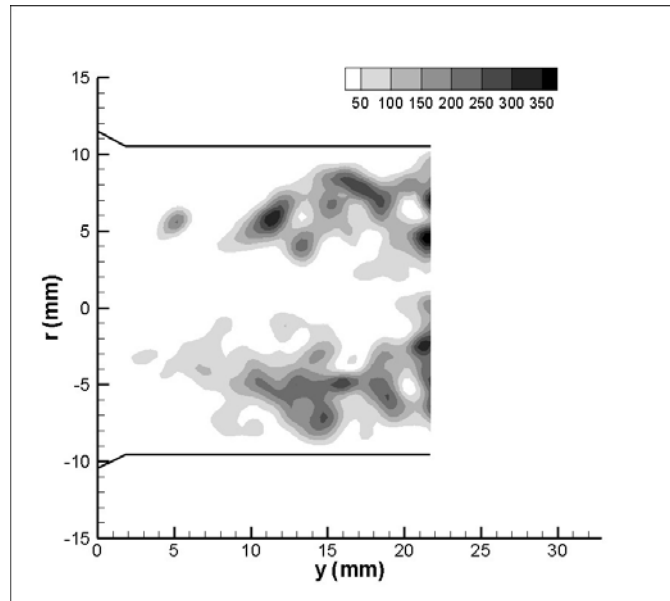

Figure B.29: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 150 ms after start of systole for open cusped diode at PVR = 6.1 mmHg/Lpm

Peak Systole (t = 350 ms)

At peak systole, a narrower jet structure is seen in the offset flow plane than in the central plane (Figure B.30). The jet flow is entrained by two recirculating regions. The peak velocity was measured at 1.8 m/s and the average velocity is 0.313 m/s. The viscous shear stress field is also seen in Figure B.30. Viscous shear stresses of 31 dynes/cm^2 are at the edges of the entrained jet. The Reynolds shear stresses peak at 857 dynes/cm^2 (Figure B.31) and occur within the vortices.

Mid Diastole (t = 550 ms)

During mid diastole the flow behaves in the off center flow plane is comparable to that in the central plane. The flow velocities have decelerated to an average velocity of 0.019 m/s with peak velocity values of 0.221 m/s. The shear stresses are low. The maximum values of hydraulic shear are throughout the field. There are three discernible shear layers observed between the diminishing jet and the retrograde flow near the walls. The peak viscous stresses are 5.1 dynes/cm^2. Figure B.33 shows that the RSS values reach a maximum at 242 dynes/cm^2.

Diastole (t =750 ms)

As was the case with the central plane, the diastolic flow in the off center plane has a uniform profile Figure B.34. Retrograde flow is predominant; thus, the average axial velocity is -0.090 m/s and it peaks at -0.416 m/s. Since the flow is evenly distributed across the offset plane cross section, the flow provides a sweeping of the

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aretery walls. The peak viscous shear stresses are 7.5 dynes/cm^2 along the walls. The Reynolds shear stresses are just as low at 39 dynes/cm^2 (Figure B.35).

Backchannel Diode - Case 2

The pressure and flow curves for the moderate PVR and RF% case for the back - channel diode are shown in Figure B.36. The PVR = 4.1 mmHg/Lpm and the RF% = 6.25. The flow rate spans from 14 Lpm to – 2.1 Lpm.

Early Systole (t =150 ms)

The central plane flow and viscous shear stress field for 150 ms after the start of systole is in Figure B.37. A jet formation present at the valve exit; however, by 10 mm downstream the axial flow profile in the MPA is uniform. The average is 0.111 m/s and the peak velocity is 0.501 m/s. The flow velocities in the left and right branches are uniformly distributed.

The shear stresses in the shear layer created by the emerging jet measure up to 11 dynes/cm^2 (Figure B.37). This is observed within the first 10 mm of the valve exit. As the flow reattaches to the wall, the shear stresses reach 5 dynes/cm^2 in the lower MPA and LPA, and 6 dynes/cm^2 in the upper MPA. There is a flow gradient along the distal RPA wall that generates shear stress 4 - 5 dynes/cm^2.

The Reynolds shear stresses are mapped in Figure B.38. They peak at 23 dynes/cm^2. The maximum turbulent stresses are located where the recirculation ends.
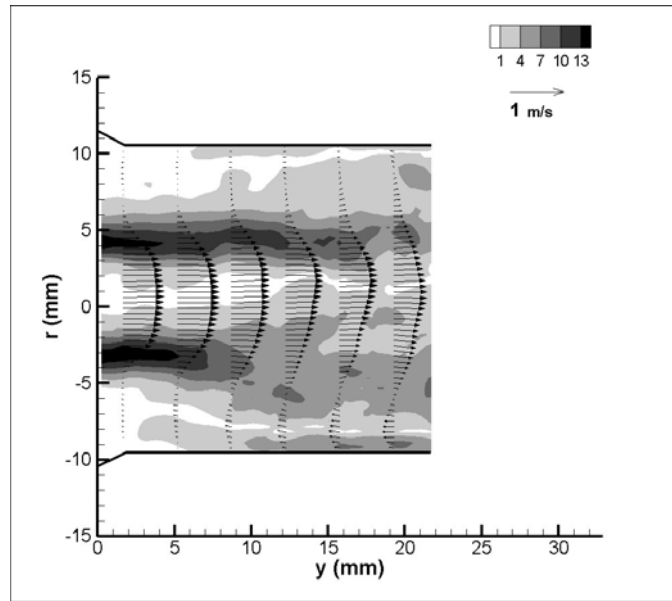
Figure B.30: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after the start of systole for PVR 6.1 mmHg/Lpm
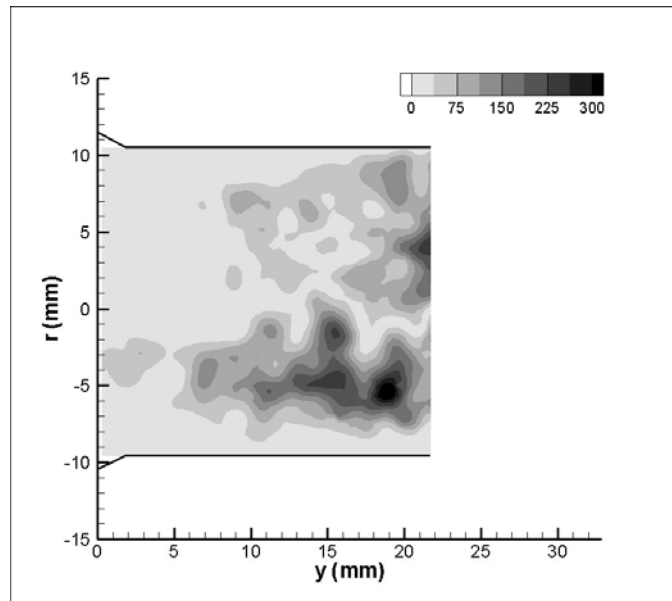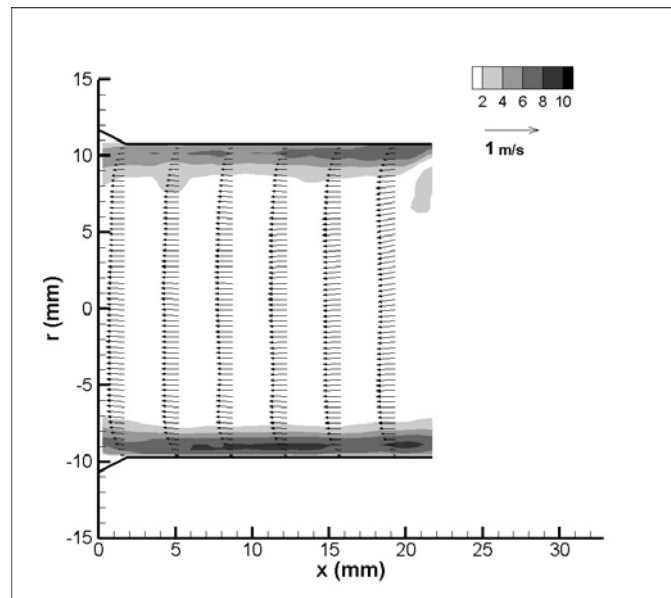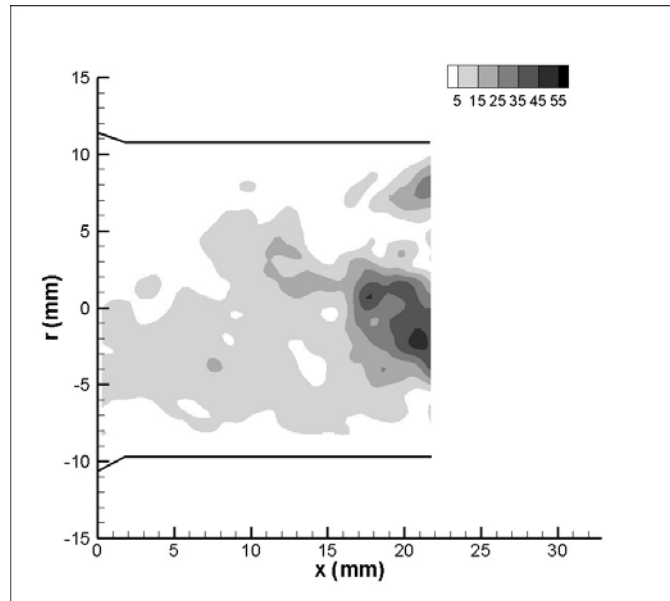

Figure B.31: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 350 ms after start of systole for open cusped diode at PVR = 6.1 mmHg/Lpm

Figure B.32: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after the start of systole for PVR 6.1 mmHg/Lpm

Figure B.33: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 550 ms after start of systole for open cusped diode at PVR = 6.1 mmHg/Lpm
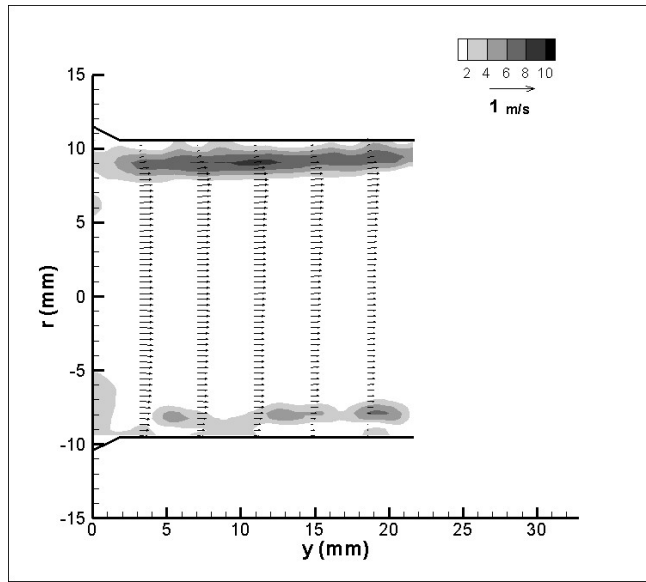
Figure B.34: Offset plane flow and viscous shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after the start of systole for PVR 6.1 mmHg/Lpm
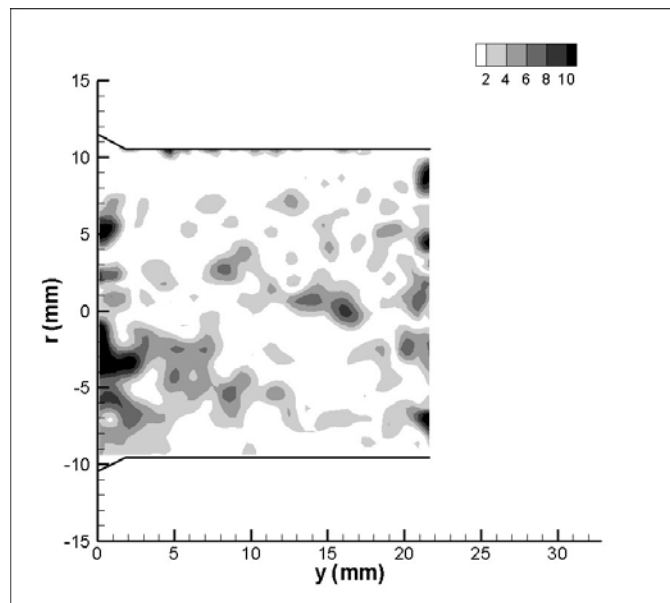

Figure B.35: Offset Reynolds shear stress (dynes/cm^2) field for the open cusped diode at 750 ms after start of systole for open cusped diode at PVR = 6.1 mmHg/Lpm
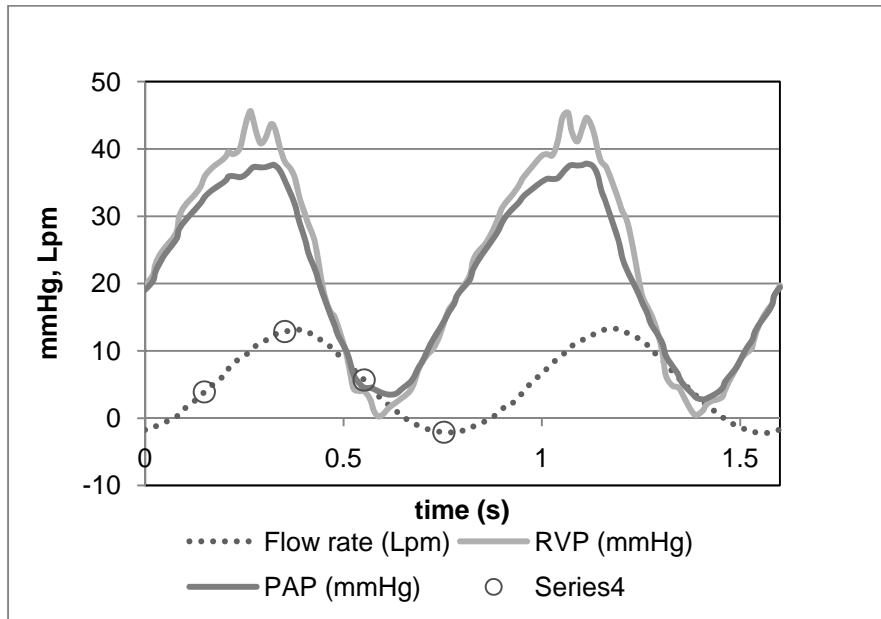
Figure B.36: Flow and pressure curve for backchannel diode at PVR
4.1 mmHg/Lpm

Peak systole (t = 350 ms)

Figure B.39 shows that during the maximum flow rate the flow patterns are similar to previous discussed patterns at this point in the cycle. A central jet develops and becomes well defined 350 ms after the start of systole. The jet travels well into the LPA and impinges on the artery wall at the bifurcation. Vortex structures surround the jet in the upper and lower MPA. An area of recirculation is carried into the RPA and the flow is skewed towards the outer wall of the RPA. The average and peak velocities are 0.517 m/s and 1.8 m/s , respectively.

The viscous shear stress field is also shown in Figure B.39. The maximum hydraulic stresses along the edges of the jet are 51 dynes/cm^2. Downstream, the values

drop to 12 dynes/cm^2. There are wall stresses along the lower MPA between $10 - 40$ mm. They measure 7 - 16 dynes/cm^2. The wall stresses along the distal RPA are as high as 27 dynes/cm^2. Also, at the site of flow impingement, the shear stresses are about 25 dynes/cm^2.

The Reynolds shear stresses for peak systole are displayed in Figure B.40. The regions of elevated Reynolds stresses begin $20 - 22$ mm downstream of the valve exit. The peak stresses are about 800 dynes/cm^2 and coincides with the region of recirculation in the lower main and left pulmonary arteries. The Reynolds shear stresses reach 250 dynes/cm^2 at the RPA bend where flow separation begins. Another area of raised turbulent shear stresses exists, up to 380 dynes/cm^2, in the RPA.

Figure B.37: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR = 4.1 mmHg/Lpm

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Figure B.38: Reynolds shear stress field (dynes/cm^2) for the backchannel diode at 150 ms after the start of systole for PVR = 4.1 mmHg/Lpm, central plane

Figure B.39: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 4.1 mmHg/Lpm

Mid diastole (t = 550 ms)

The decelerating flow field for Case 2 is shown in Figure B.41. The central jet structure is still seen. The peak velocities in the MPA are 0.794 m/s, less than one half of the peak speeds at 350 ms. The average axial velocity is 0.228 m/s.

The corresponding viscous shear stresses are also mapped in Figure B.41. The peak stresses along the edges of the jet measure 20 dynes/cm^2. The RPA distal wall stresses were between 9 and 13 dynes/cm^2.

Figure B.42 maps the Reynolds shear stresses for the moderate PVR case. The higher turbulent shear stresses occur in the areas of mixing in the lower LPA and MPA and just at the branch between the MPA and RPA. In the lower region, the peak stresses measure 540 dynes/cm^2. In the upper region, the peak stresses are 310 dynes/cm^2, which is higher than the observed stresses in the this area at t = 350 ms.

Figure B.40: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 4.1 mmHg/Lpm, central plane
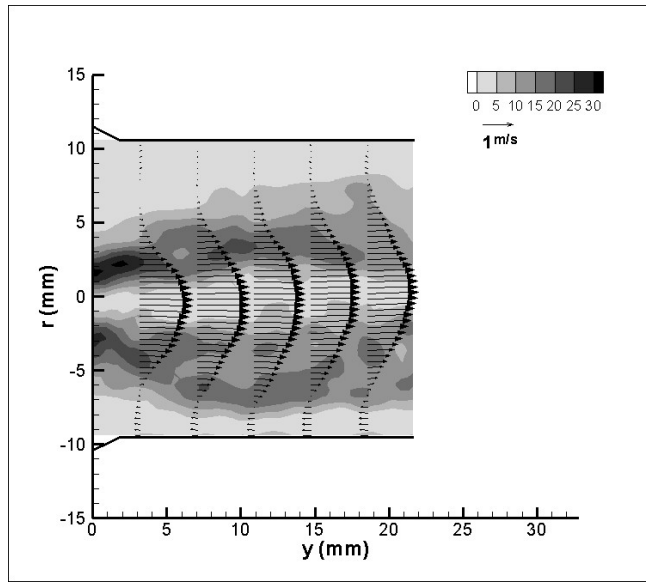

Figure B.41: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR = 4.1 mmHg/Lpm
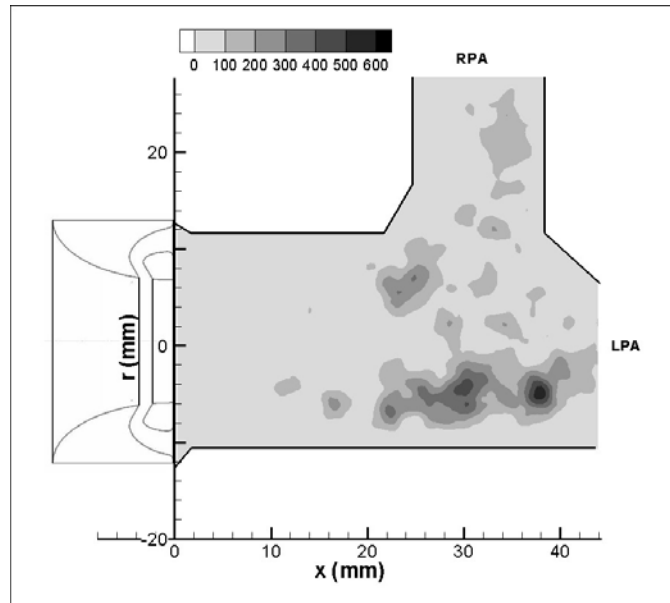
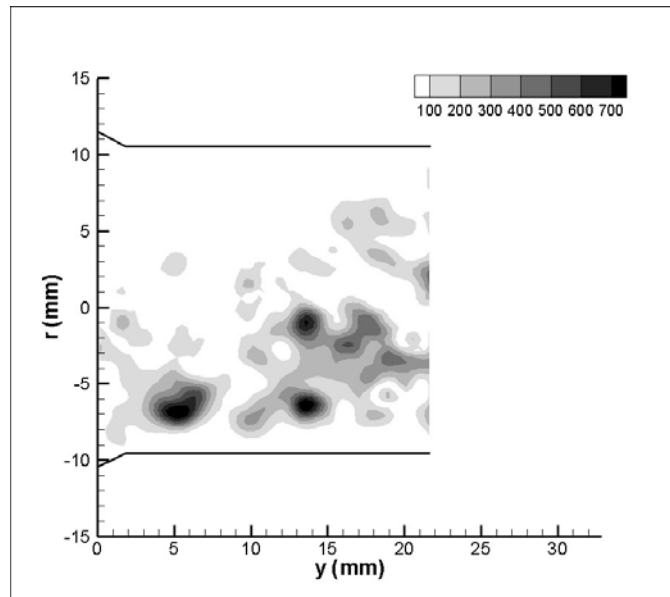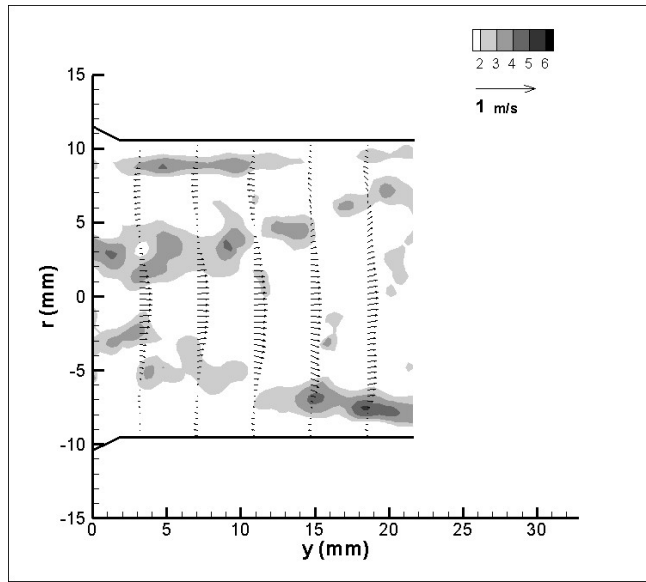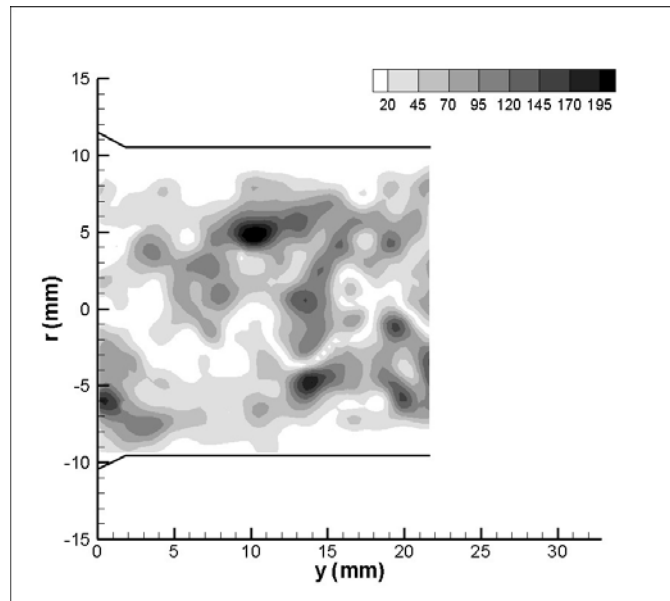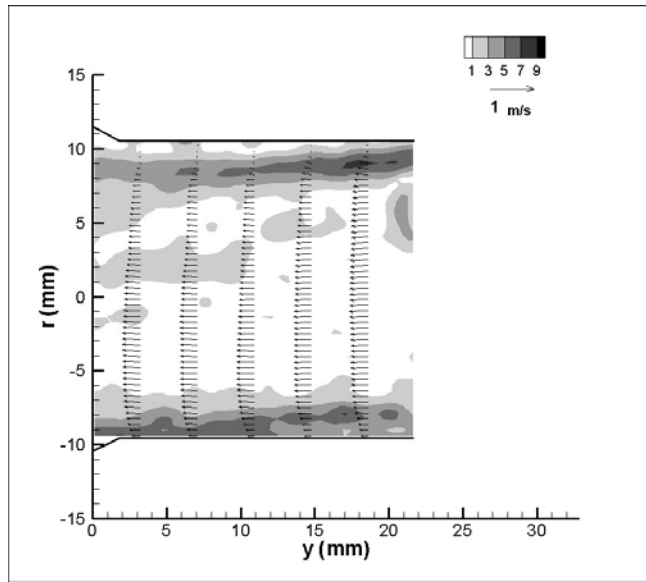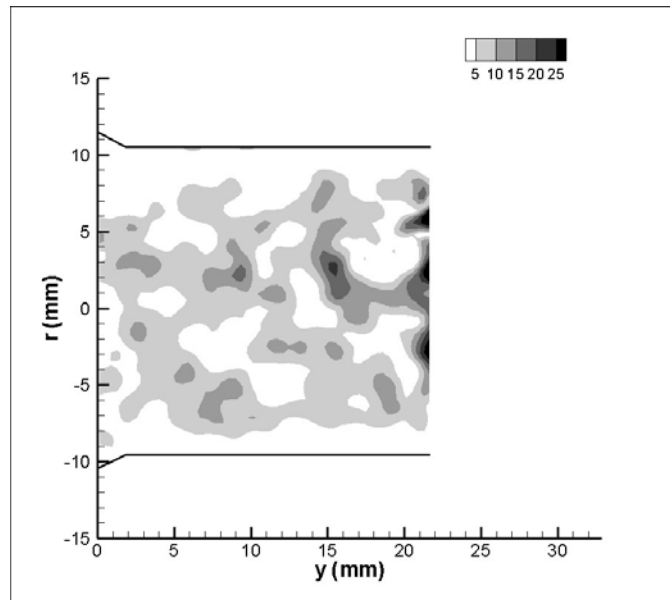Figure B.42: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR = 4.1 mmHg/Lpm, central plane

Diastole (t = 750 ms)

The diastolic flow and viscous shear stress profiles are shown in Figure B.43. Retrograde flow exists and the profile is uniform in the MPA The secondary flows from the RPA and LPA are reentering the primary flow. These flows meet at the bifurcation and this causes the flow in the LPA to be skewed towards the lower wall. . The peak flow speed in the MPA is -0.186 m/s, and the average flow speed is -0.052 m/s.

The maximum viscous shear stresses are along the walls of the main and left pulmonary arteries. The values are low, measuring no higher than 4 dynes/cm^2.

In Figure B.44, the Reynolds shear stress field shows low levels of turbulence within the field. The maximum Reynolds shear stresses are 45 dynes/cm^2. This is located where the retrograde from both branches mix in the MPA.

Backchannel Diode Case 2 - Offset Plane

Early Systole (t = 150 ms)

At 150 ms after the start of the cardiac cycle, the developing jet is visible as seen in Figure B.45. The span of the jet is expected smaller than in the central plane. As with the central plane flow, the flow takes on a more uniform profile by 8 mm downstream of the valve exit. The peak axial velocity is 0.513 m/s. The average is 0.111 m/s. The viscous shear stresses at t = 150 ms in the offset plane are of similar location and magnitude as in the central plane (Figure B.45). There is a shear layer that exists at the edges of the jet exiting the valve orifice. The peak bulk flow shear stresses are around 12 dynes/cm^2. The wall stresses are between 3-5 dynes/cm^2. The Reynolds shear stresses are very low (Figure B.46). The maximum RSS measure 13 dynes/cm^2.

Peak Systole (t = 350 ms)

The flow mapping for the offset plane during peak systole shows a central jet that travels the length of MPA shown in Figure B.47. Two areas of recirculation surround the jet. The peak velocities are 1.67 m/s, less than in the central plane. The average flow speed is 0.354 m/s. The maximum viscous shear stresses are around 45 dynes/cm^2; they are the same in this plane as they were in the central plane (Figure B.47). Likewise, the peak stresses are along the edges of the jet. Since the plane of view only covers 22 mm

downstream of the valve, the wall shear along the lower MPA and LPA walls do not appear in this stress field.

Figure B.48 shows the Reynolds shear stresses for this plane. The RSS measurements are overall very low. The upper MPA area, the turbulent shear stresses are less than 10 dynes/cm^2. In the lower region, they measure up to 50 dynes/cm^2. At the edge of the field of view, there is an isolated region of relatively high turbulent shear stresses (300 dynes/cm^2). This corresponds to the beginning of the recirculation area in the lower MPA.

Mid Diastole (t= 550 ms)

During mid diastole, the jet structure is seen to weaken as it did in the central plane (Figure B.49). The maximum and average velocities are 0.656 m/s and 0.123 m/s, respectively. The bulk flow shear stresses are highest along the edges of the central flow stream as seen in Figure B.49. The peak values are 15 dynes/cm^2. The shear layer widen as the jet dissipates. By 22 mm downstream, the shear stresses are down to 4 dynes/cm^2.

Figure B.50 is the mapping of the turbulent shear stresses for the offset plane. This map follows a similar trend as the central plane field. The highest stresses are 5 mm below the centerline between 10 and 22 downstream. This is consistent with the RSS field in the central plane in Figure B.42. The peak RSS measurements are 275 dynes/cm^2.
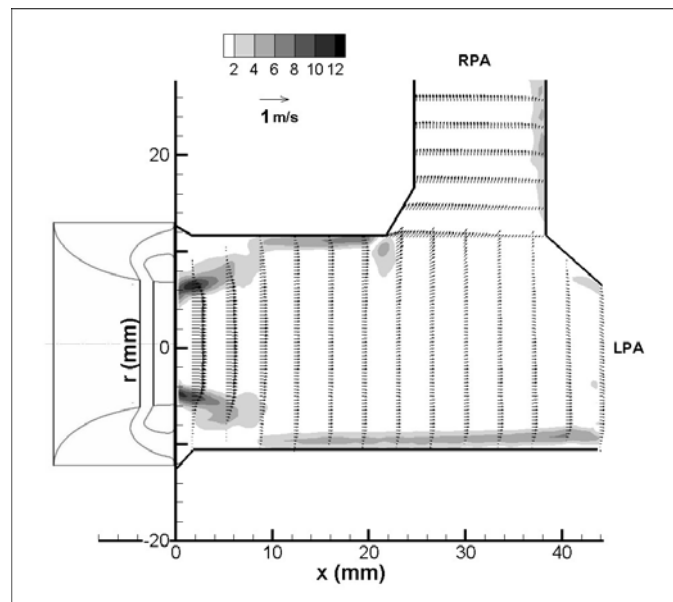
Figure B.43: Central plane flow and viscous shear stress (dynes/cm^2) field for
the backchannel diode at 750 ms after the start of systole for PVR = 4.1
mmHg/Lpm

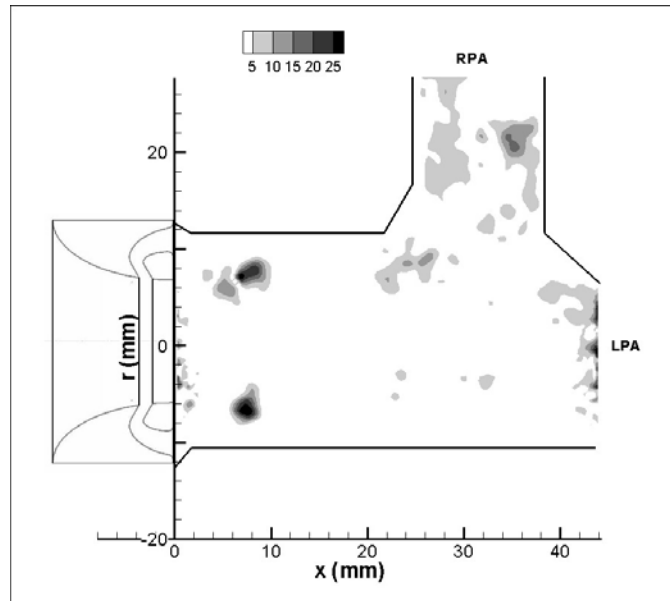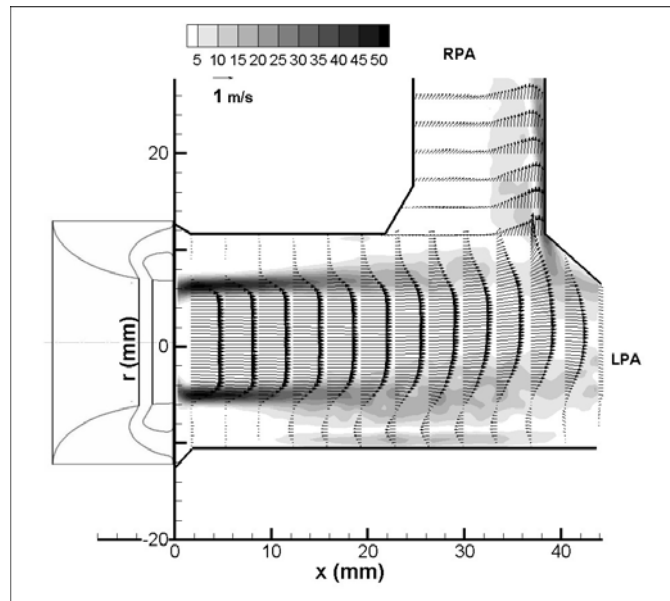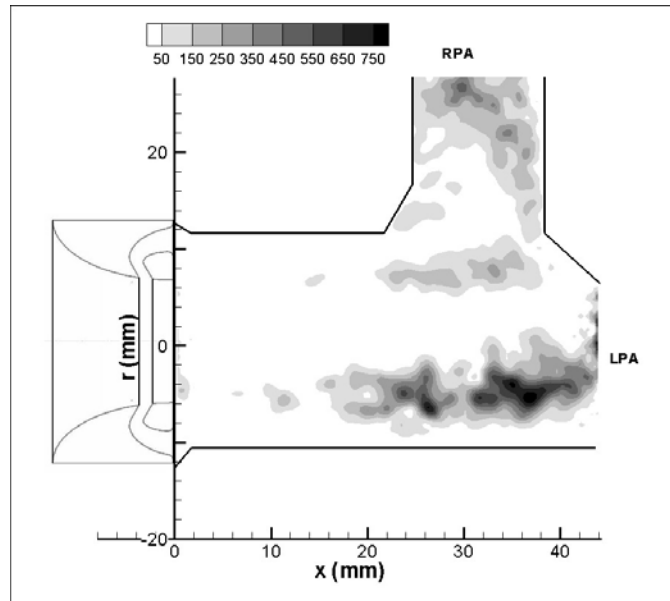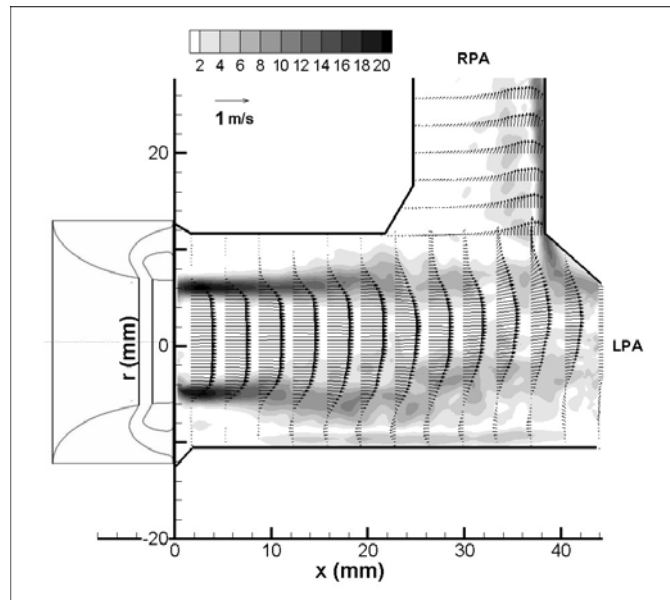Figure B.44: Reynolds shear stress (dynes/cm^2) field for the backchannel
diode at 750 ms after the start of systole for PVR = 4.1 mmHg/Lpm
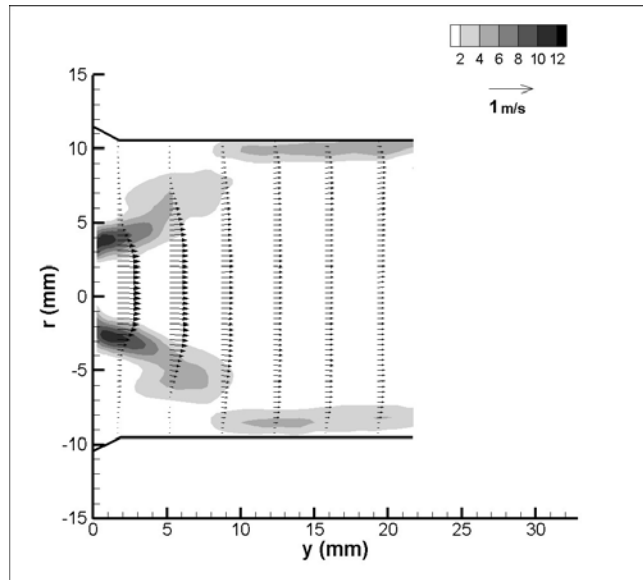
Figure B.45: Offset plane flow and viscous shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm
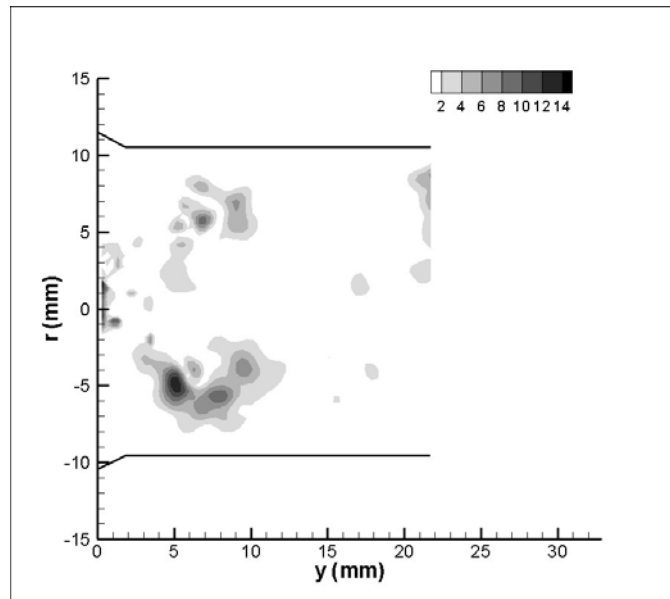
Figure B.46: Offset Reynolds shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm
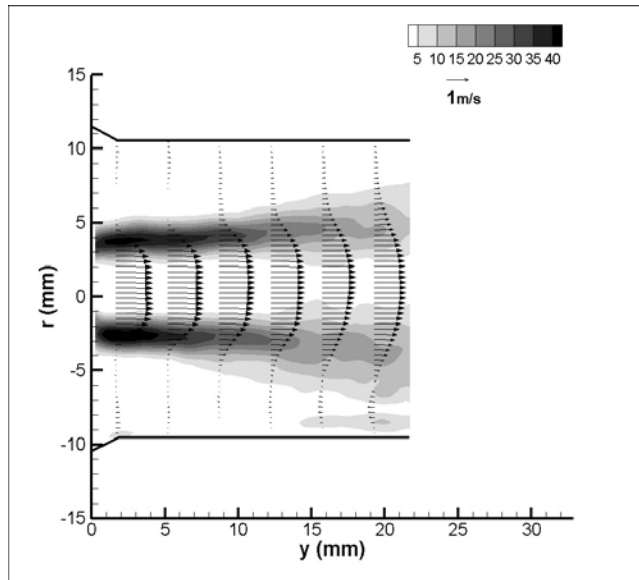
Figure B.47: Offset plane flow and viscous shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm

Late Diastole (t= 750 ms)

The offset plane flow and viscous shear stress data during diastole is shown in Figure B.51. Uniformly distributed retrograde flow exists; thus, the flow provides a thorough sweep of the walls. The peak velocity is -0.125 m/s and the mean velocity is -0.037 m/s. The viscous shear stresses along the wall measure between 1.5 - 4 dynes/cm^2.

Figure B.52 shows the turbulent shear stresses at 750 ms after the start of systole. The RSS values are very low in comparison to the other time steps. The maximum turbulent shear stress magnitudes are 15 dynes/cm^2.
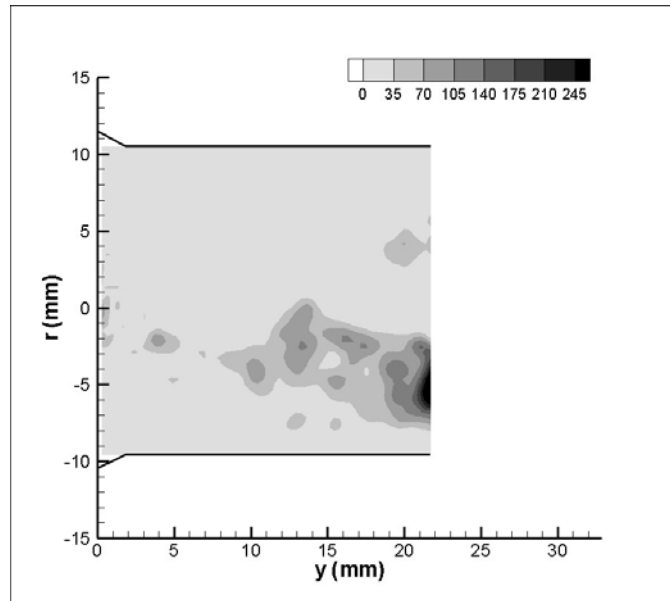
Figure B.48: Offset Reynolds shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm
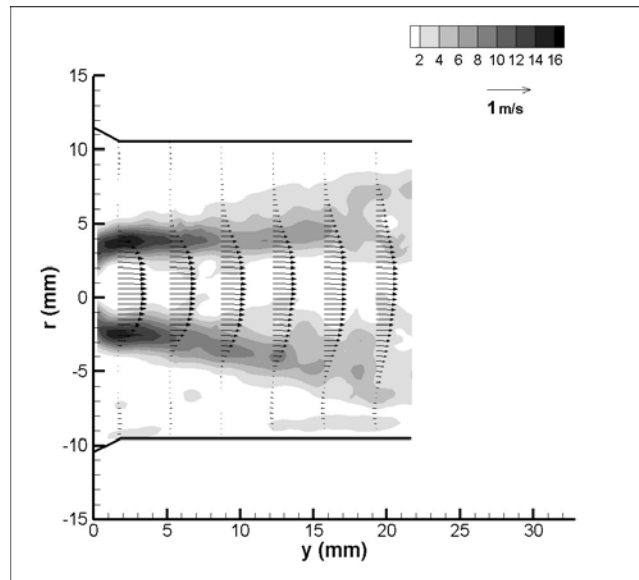
Figure B.49: Offset plane flow and viscous shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm

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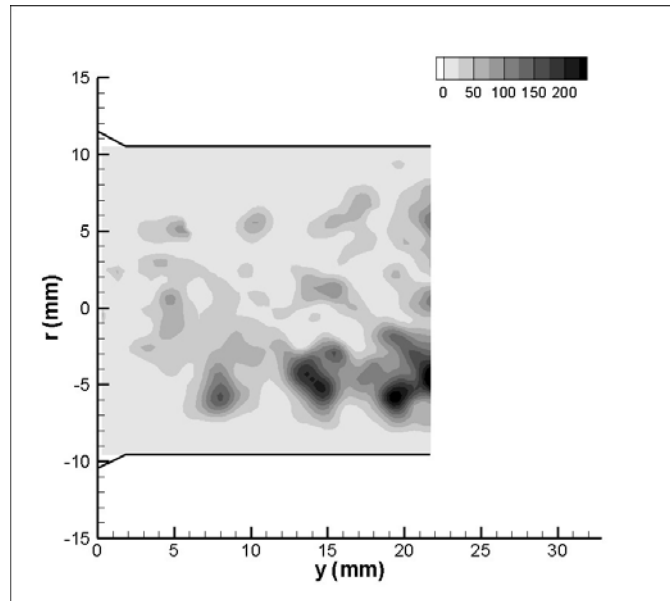
Figure B.50: Offset Reynolds shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm
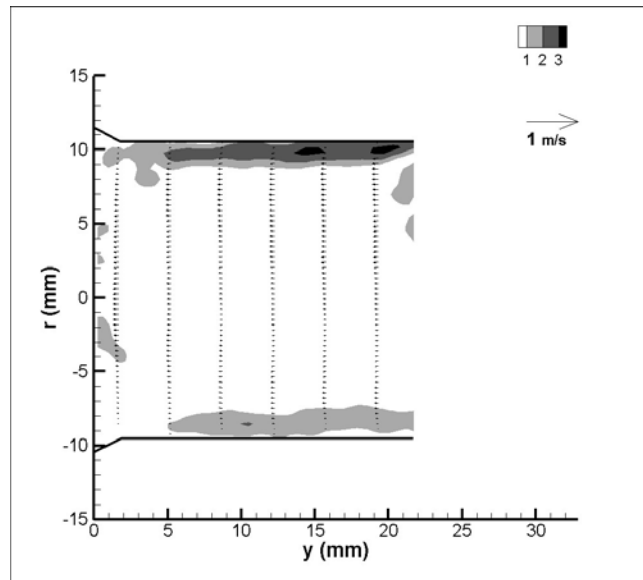
Figure B.51: Offset plane flow and viscous shear stress (dynes/cm^2) field at 750 ms after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm

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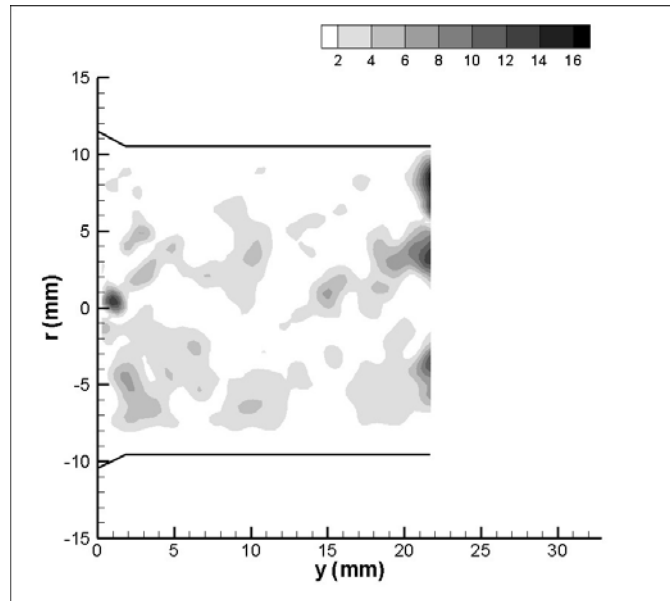
Figure B.52: Offset Reynolds shear stress (dynes/cm^2) field at 750 ms
after start of systole for backchannel diode at PVR = 4.1 mmHg/Lpm

Backchannel Diode - Case 3

The flow and pressure curve for the PVR = 5.1 mmHg/Lpm is shown in Figure B.53. The regurgitant fraction is 15.0%.

Early Systole (t =150 ms)

At 150 ms after the start of systole, there is uniform, low magnitude antegrade flow (Figure B.54). There is a complete pass of the artery walls. The average axial velocity 0.059 m/s and the peak velocity is 0.196 m/s.

The viscous shear stresses are also mapped in Figure B.54. The stresses are highest along the wall measuring 5 dynes/cm^2 in the lower LPA. In the main and right pulmonary arteries, the stresses are around 2 - 3 dynes/cm^2.

Figure B.55 is the mapping of the Reynolds shear stresses 150 ms after the start of the cardiac cycle. The turbulent stresses are overall very low. There are between -15 and 55 dynes/cm^2. The peak RSS is at the exit of the RPA.
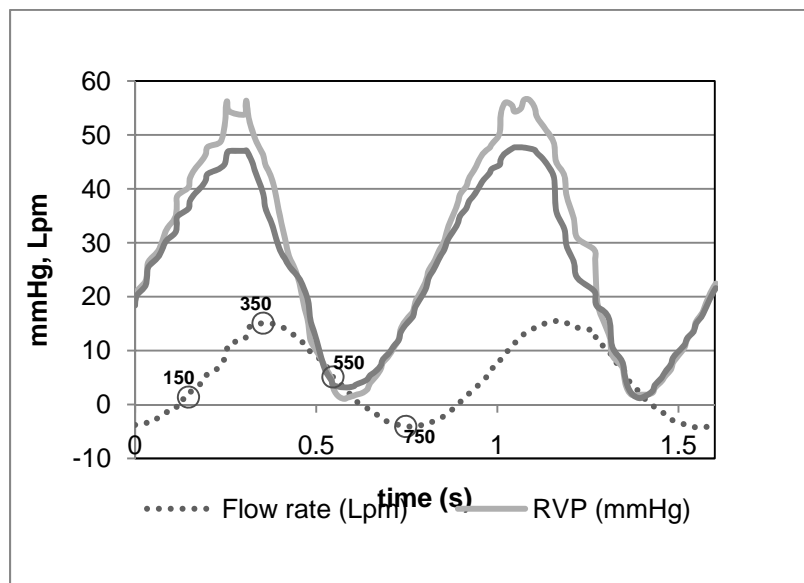
Figure B.53: Flow and Pressure Curve for backchannel diode at
PVR = 5.1 mmHg/Lpm

Figure B.54: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR =5.1 mmHg/Lpm

Figure B.55: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR = 5.1 mmHg/Lpm

Peak systole (t = 350 ms)

The flow and viscous shear stresses at peak systole are in Figure B.56. A strong central jet emerges from the valve exit and is best seen in Figure B.56. The jet impinges on the artery wall at the bifurcation. There is an area of recirculation in the lower MPA and LPA. Another area is in RPA entrance. The flow along the distal RPA wall is pronounced as well. The peak velocities within the jet reach 2.07 m/s and the average velocity in the MPA is 0.611 m/s.

The bulk flow shear stresses are high along the edges of the jet (Figure B.56), at the lower MPA and LPA walls, and along the distal RPA wall. The maximum shear stresses are 62 dynes/cm^2 at the beginning of the jet stream. The wall stresses in the RPA are between 34 - 43 dynes/cm^2 and up to 17 dynes/cm^2 at the lower MPA and LPA walls.

Figure B.57 maps the RSS values for the peak systole case. There is a region in the lower MPA in the area of recirculation. The peak RSS measurements here are up to 1100 dynes/cm^2. Another area of high turbulence is in the upper MPA near the where flow enters the RPA. The RSS values are as high as 690 dynes/cm^2. Finally, in the right pulmonary artery, there is also a region of elevated stresses ranging up to 490 dynes/cm^2.
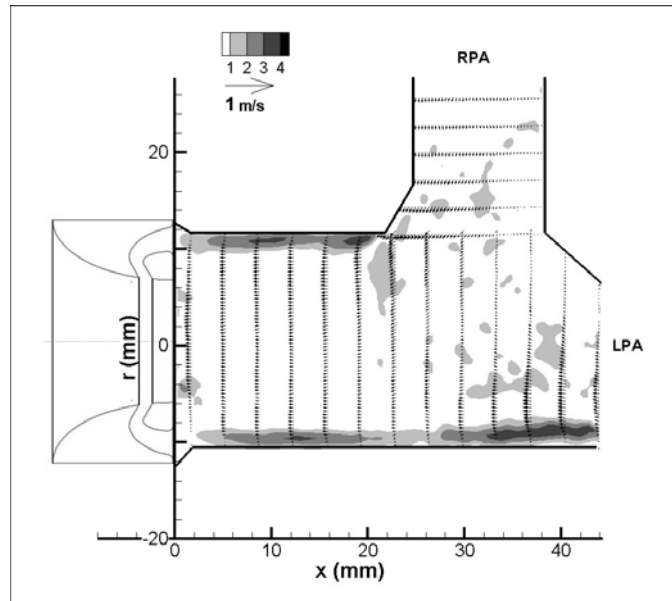
Figure B.56: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 5.1 mmHg/Lpm
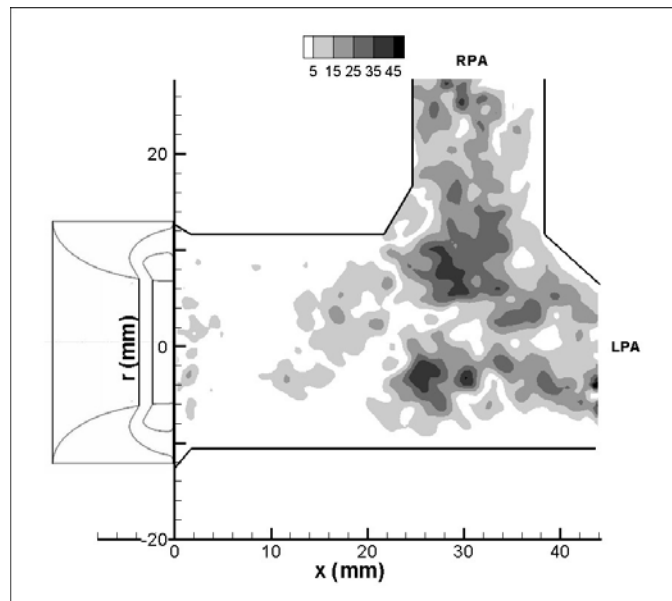

Figure B.57: Central plane Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR = 5.1 mmHg/Lpm

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Mid Diastole (t = 550 ms)

Figure B.58 displays the flow and hydraulic shear stress fields for the mid diastole phase (t = 550 ms). A jet stream from the valve orifice is still visible as a region of flow recirculation is seen in the lower pulmonary artery. The flow gradient in the RPA is lessening. Additionally, the reverse velocity vectors along the lower LPA and MPA walls are stronger than during peak systole. The maximum flow speeds at 550 ms are roughly half of that measured during peak systole. The peak velocity is 0.981 m/s and the average is 0.283 m/s.

The hydraulic shear stresses are highest at the outer RPA walls, in the area where the jet flow encounters the artery wall at the bifurcation, and (Figure B.58). The peak viscous shear stresses are again along the edges of the jet. The wall stresses in the RPA are between 15-20 dynes/cm^2 while the stresses at the site of impingement are around 12 dynes/cm^2.

Figure B.59 shows the Reynolds shear stresses in the decelerating flow field. The RSS measured up to 750 dynes/cm^2. The peak RSS measurements are around 750 dynes/cm^2 and are located in the vortical structure near the lower MPA wall.

Figure B.58: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR = 5.1 mmHg/Lpm

Figure B.59: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR = 5.1 mmHg/Lpm

Late Diastole (t = 750 ms)

The flow field during diastole for Case 3 is uniformly distributed retrograde flow (Figure B.60). In the LPA, the flow is slightly skewed to the lower side. This is a result of the momentum from the flow from the secondary flows meeting and creating an area of stasis near the artery branch. The average velocity in the MPA is -0.088 m/s with velocity reaching maximums at -0.273 m/s.

The uniform flow sweeps the artery walls. This causes elevated wall stresses along the MPA walls as well as the lower LPA wall and distal RPA wall (Figure B.60). The peak wall stresses are in the LPA at 8 dynes/cm^2. In the main artery, the wall stresses are just below 5 dynes/cm^2 and the wall stresses along the outer RPA are between 3 – 4 dynes/cm^2. There is also a shear layer between the two secondary flow streams when they converge in the MPA. This shear layer results in bulk flow shear stresses of around 4 dynes/cm^2.

The overall Reynolds shears stresses during diastole are less than 100 dynes/cm^2 (Figure B.61). The area of higher turbulent shear stresses coincides with the mixing layer of the two secondary flows. The RSS are between 50 -75 dynes/cm^2 in this location.

Figure B.60: Central plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 750 ms after the start of systole for PVR = 5.1 mmHg/Lpm

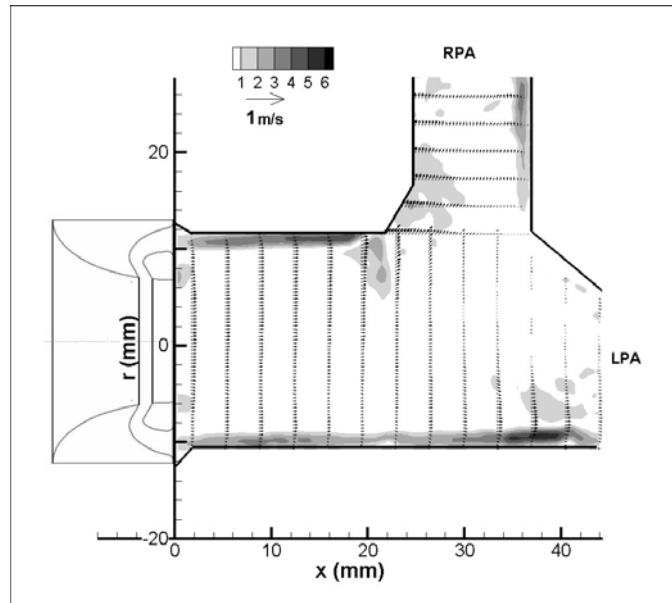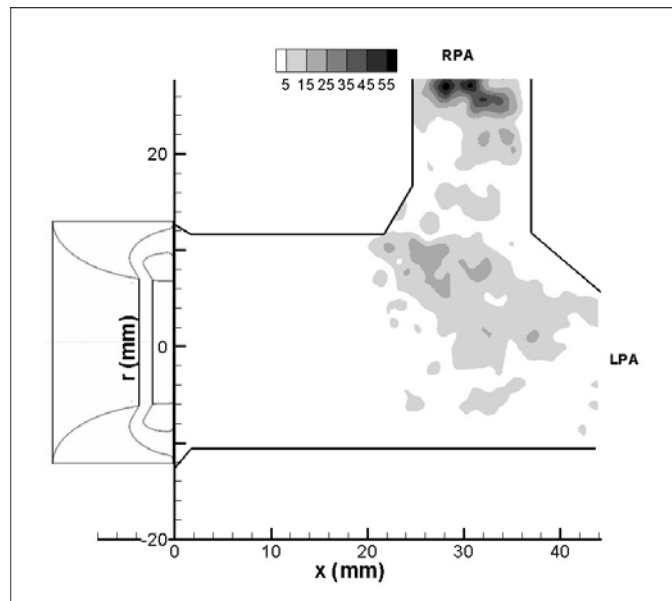Figure B.61: Reynolds shear stress (dynes/cm^2) field for the backchannel diode at 750 ms after the start of systole for PVR = 5.1 mmHg/Lpm, central plane

Backchannel Diode Case 4 - Offset Plane

Early Systole (t = 150 ms)

As the flow begins to accelerate, there is little movement in the flow Figure B.62. The average speed is -0.036 m/s and the peak is -0.08 m/s. The highest viscous stresses are at the lower MPA wall with magnitudes up to 4.2 dynes/cm^2. In Figure B.63 it is seen that the stagnant flow leads to little mixing. The turbulent shear stress levels are below 25 dynes/cm^2. Peak Systole (t = 350 ms)

The offset flow field at peak systole is shown in Figure B.64. The width of the jet has narrowed just as the width of the valve orifice is smaller in this plane. There is an area of recirculation in the lower half of the section. Retrograde flow appears nearest the valve exit. The axial velocities reach 0.291 m/s on average with peaks of 1.19 m/s.

The bulk flow shear stresses follow the shear layer created by the entrained jet. The peak shear stresses measure 17.6 dynes/cm^2. Also, along the wall where the vortex is sweeping back the walls, the wall stresses reach 10 dynes/cm^2.

The Reynolds shear stresses peak at 283 dynes/cm^2 in the offset flow field for this case (Figure B.65). The highest values are contained in the shear layer created by the offset jet structure.

Mid Diastole (t = 550 ms)

During the mid diastole, as with Early Systole, there is little activity in the offset flow field (Figure B.64). The velocities have low magnitudes. The peak speed is 0.280

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m/s and the average is 0.034 m/s. The jet structure is still visible, albeit small. The flow along both the upper has reversed so that there is retrograde flow in the outer radial position. The flow within the first 8 mm of the valve is also flowing back to the valve. The maximum viscous shear stress is 7.7 dynes/cm^2 and is located 18 mm downstream along the wall.

Figure B.65 shows the Reynolds shear stresses; these values for the offset field of view reach a maximum at 136 dynes/cm^2.

Late Diastole (t =750 ms)

Figure B.68 maps the velocity and hydraulic shear stress fields for the final case during diastole. Just as it was in the central plane of flow, the velocity profile is uniform. The average axial flow speed is -0.304 m/s. and the peak speed is -0.580 m/s. The highest viscous shear stresses measure 14.3 dynes/cm^2. The shear stresses along the walls are higher than those in the flow field.

Figure B.69 maps the RSS field as it occurs during diastole. The highest turbulent shear stresses are 95 dynes/cm^2 and are located 22 mm downstream.
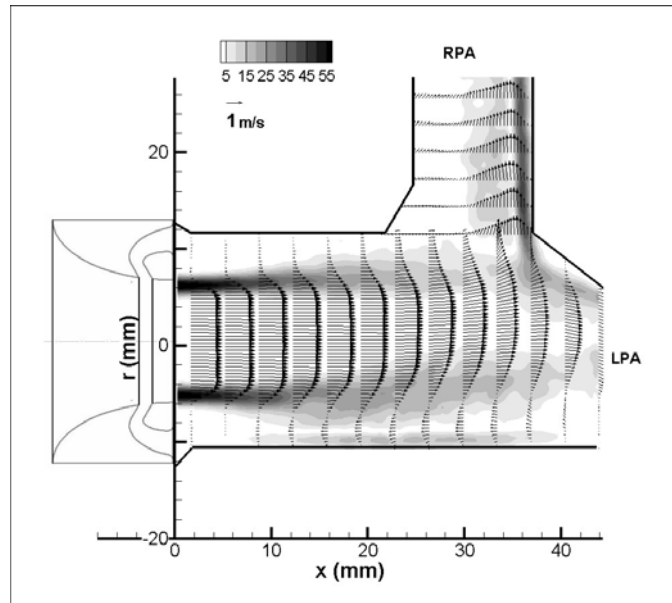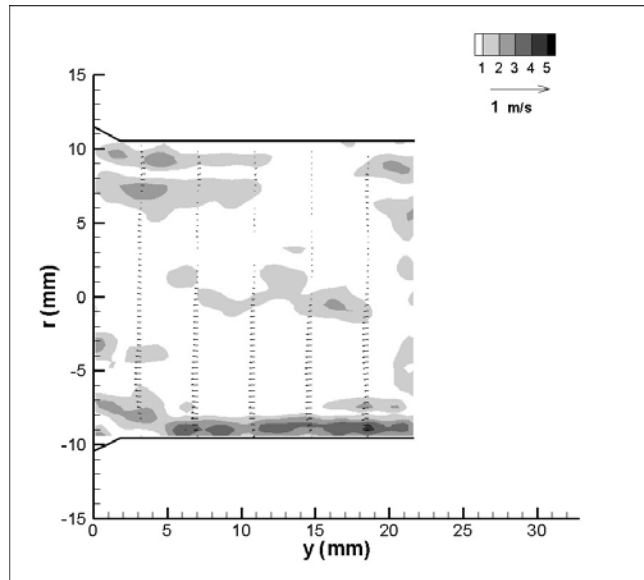
Figure B.62: Offset plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 150 ms after the start of systole for PVR 6.9 mmHg/Lpm
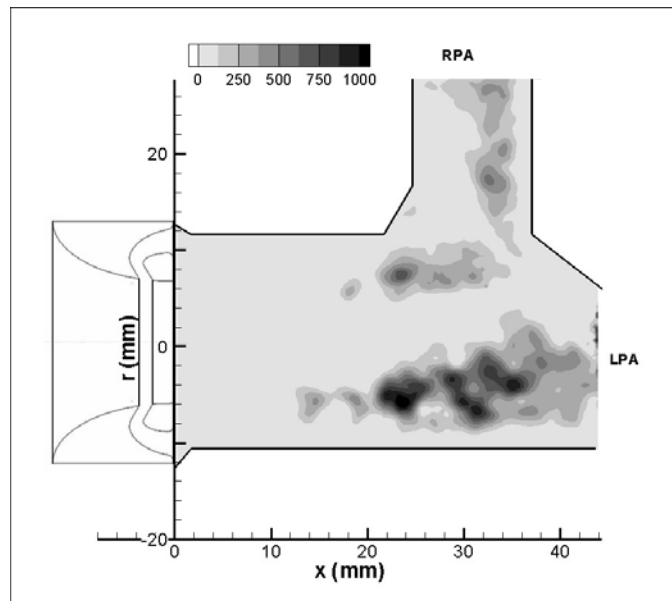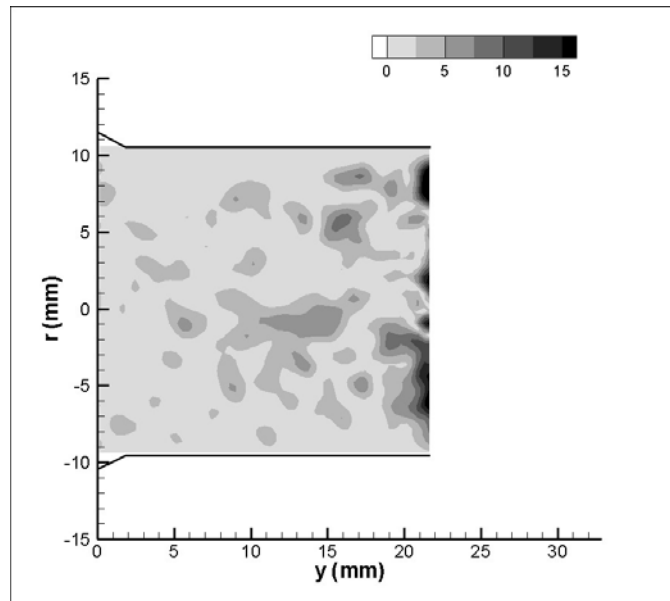

Figure B.63: Offset Reynolds shear stress (dynes/cm^2) field at 150 ms after start of systole for backchannel diode at PVR = 6.9 mmHg/Lpm
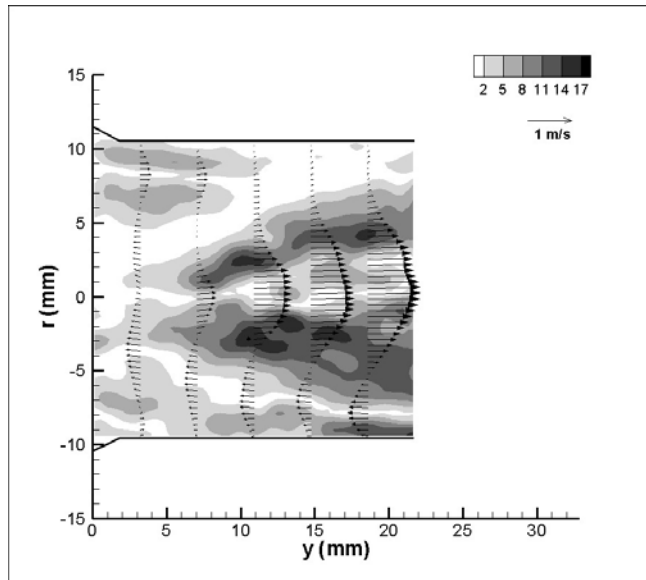
Figure B.64: Offset plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 350 ms after the start of systole for PVR 6.9 mmHg/Lpm
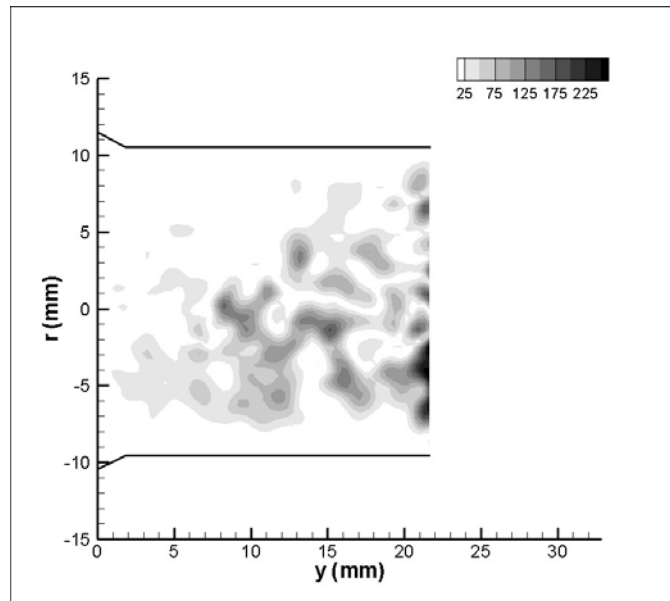
Figure B.65: Offset Reynolds shear stress (dynes/cm^2) field at 350 ms after start of systole for backchannel diode at PVR = 6.9 mmHg/Lpm
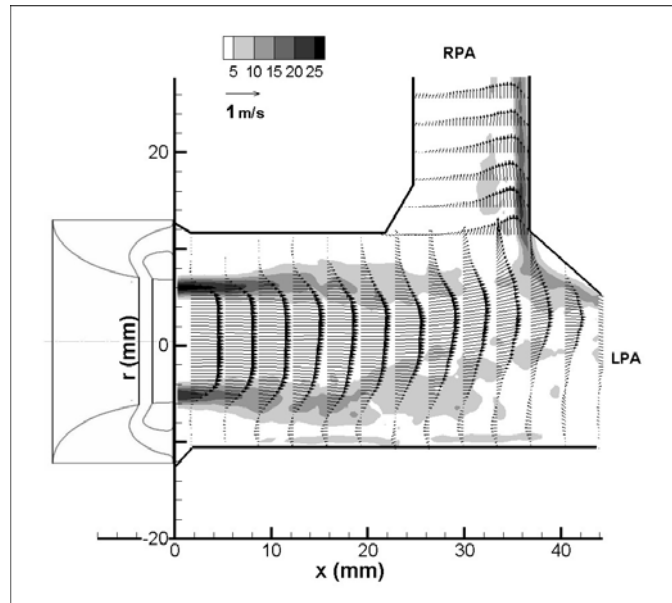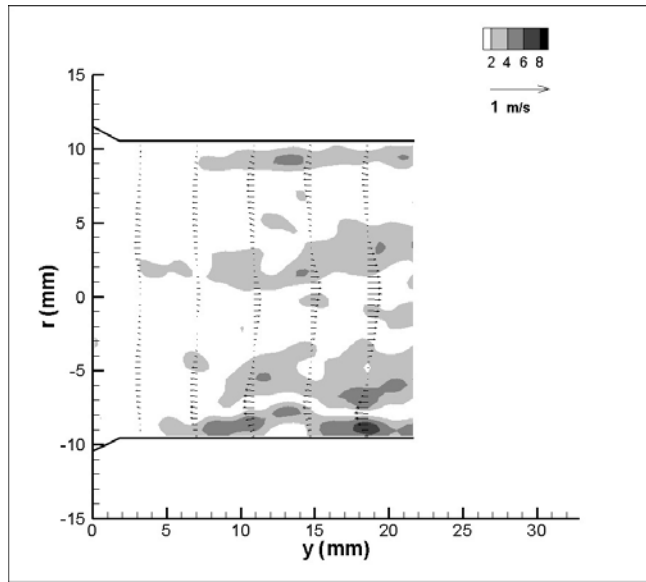
Figure B.66: Offset plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 550 ms after the start of systole for PVR 6.9 mmHg/Lpm
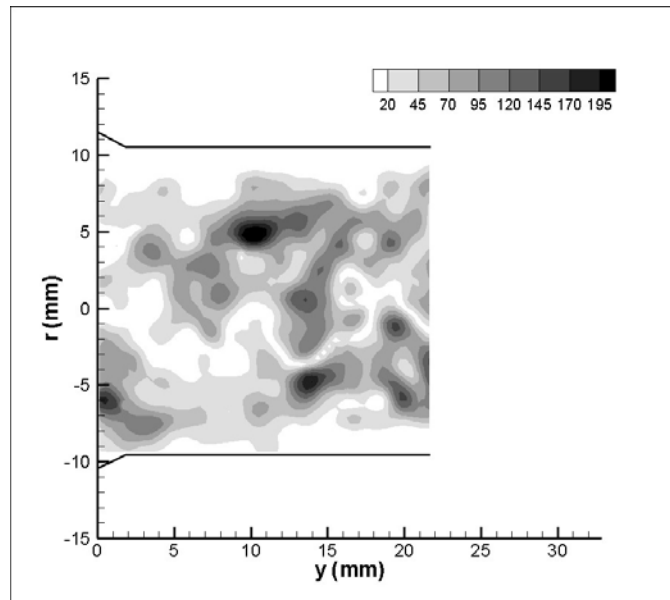
Figure B.67: Offset Reynolds shear stress (dynes/cm^2) field at 550 ms after start of systole for backchannel diode at PVR = 6.9 mmHg/Lpm
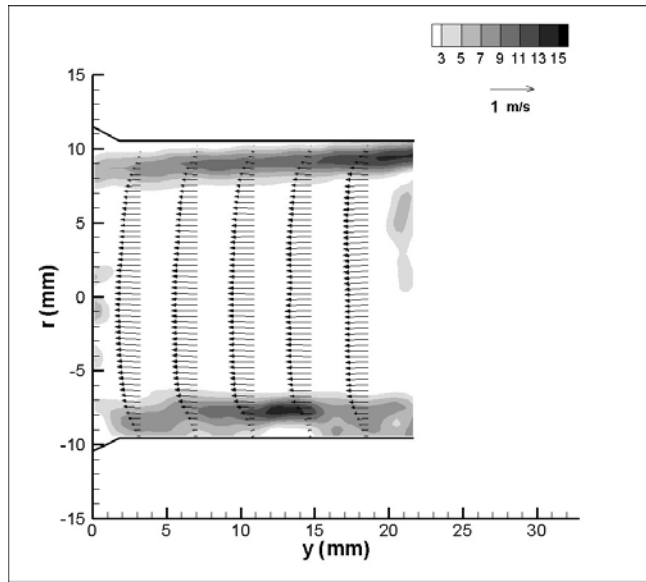
Figure B.68: Offset plane flow and viscous shear stress (dynes/cm^2) field for the backchannel diode at 750 ms after the start of systole for PVR 6.9 mmHg/Lpm
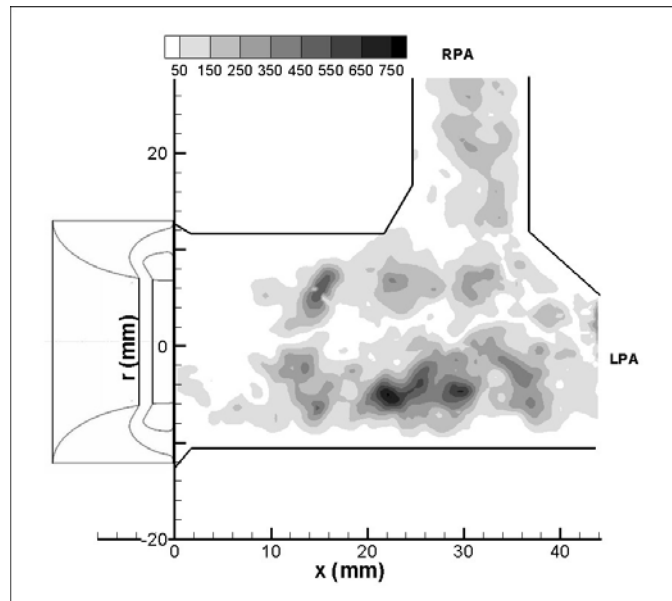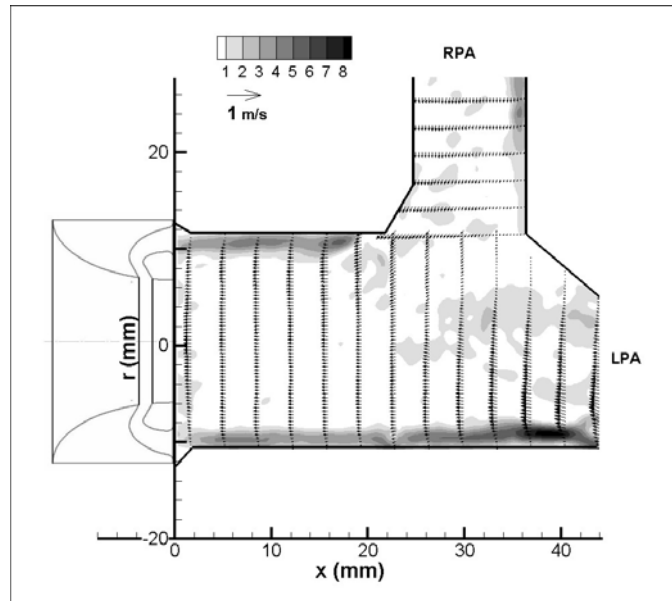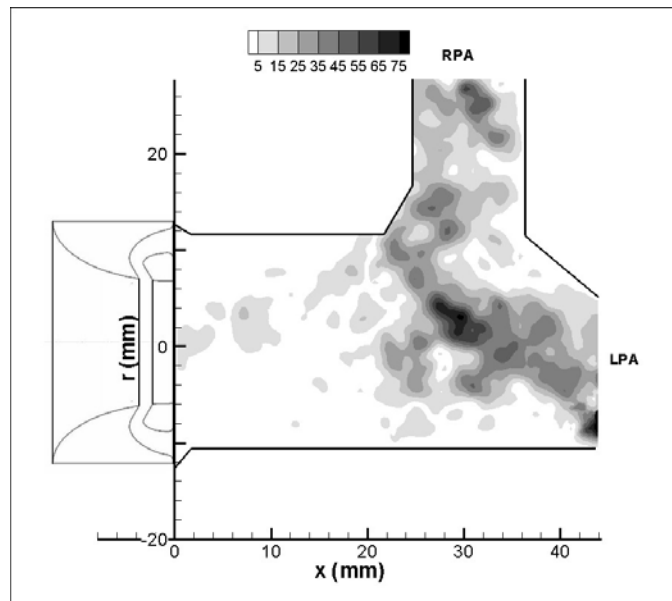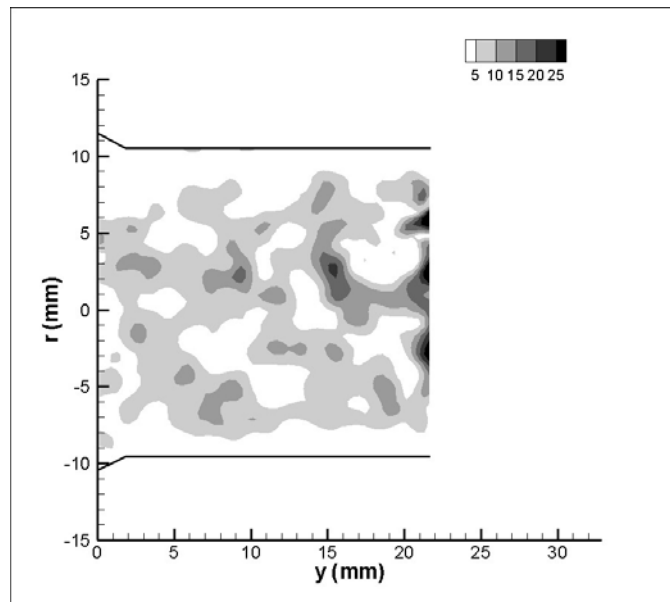

Figure B.69: Offset Reynolds shear stress (dynes/cm2) field at 750 ms after start of systole for backchannel diode at PVR = 6.9 mmHg/Lpm

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Appendix C

Uncertainty Analysis

This section reports on the uncertainty estimates for results presented in this dissertation. Elemental errors were identified for each measurement and uncertainties assigned. Uncertainties were propagated based on the methods detailed in Figliola and Beasley [123] and ASME PTC 19.1 [124]. In general, for k = 1, 2,... elemental systematic errors, systematic uncertainties are propagated as

$$b = \left(\sum_k (\theta b_k)\right)^{\frac{1}{2}} \qquad\qquad C.1$$

where θ is the sensitivity factor. In a similar manner, random uncertainties were propagated as

$$s = \left(\sum_k (\theta s_k)\right)^{\frac{1}{2}} \qquad\qquad C.2$$

with degrees of freedom estimated from the Welch-Sattertwaite formula [124].

Uncertainty in Pressure and Flow Rate Measurements

The contributing source errors to the pressure uncertainty measurements include: a systematic error based on the manufacturer's specification, which is assigned standard systematic uncertainty b; the random error resulting from calibration curve fit, assigned standard random uncertainty $s_1 = s_{yx}$ based on the standard error of the curve fit; and the variation among the multiple data measurements, assigned standard random uncertainty $s_2 = \frac{s}{\sqrt{N}}$ or the standard deviation of the mean of the pressure measurement.

The systematic (b_{RVP}) and random uncertainties (s_{RVP}) in the RVP measurement were found to be ±0.192 mmHg and ±0.199 mmHg, respectively. Likewise, the uncertainties in the PAP measurement, b_{PAP} and s_{RVP}, were ±0.192 mmHg and ±0.204 mmHg. The systematic uncertainty (b_Q) in the flow rate measurement was calculated as 0.050 Lpm. The random uncertainty (s_Q) in the flow rate measurement was calculated as 0.126 Lpm. These are shown in Table C. 1.

Uncertainty in TVG and RF% Measurements

Transvalvular Pressure Gradient

Recall that equation 3 states the relationship between the TVG and RVP and PAP as TVG = RVP$_\text{peak}$ - PAP$_\text{peak.}$ First, the systemic and random error uncertainties were found using equations C.3 – C.4.

$$b_{TVG} = \pm\sqrt{\left(\frac{\partial TVG}{\partial RVP}b_{RVP}\right)^2 + \left(\frac{\partial TVG}{PAP}b_{PAP}\right)^2} \qquad \text{C.3}$$

$$s_{TVG} = \pm\sqrt{\left(\frac{\partial TVG}{\partial RVP}s_{RVP}\right)^2 + \left(\frac{\partial TVG}{PAP}s_{PAP}\right)^2} \qquad \text{C.4}$$

Regurgitant Fraction

The systematic and random uncertainties in the RF% (defined in Equation 2) resulting from measurement error was found using equations C.5 and C.6.

$$b_{RF\%} = \pm\sqrt{\left(\frac{\partial RF\%}{\partial Q_r}b_{Q_r}\right)^2 + \left(\frac{\partial RF\%}{\partial Q_f}b_{Q_f}\right)^2} \qquad \text{C.5}$$

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$$s_{RF\%} = \pm\sqrt{\left(\frac{\partial RF\%}{\partial Q_r} s_{Q_r}\right)^2 + \left(\frac{\partial RF\%}{\partial Q_f} s_{Q_f}\right)^2} \qquad \text{C.6}$$

Pulmonary Vascular Resistance and Compliance

Equations C.6 and C.7 were used to find the uncertainties in the PVR and PVC (defined in Equations 6 and 7).

$$b_{PVR} = \pm\sqrt{\left(\frac{\partial PVR}{\partial CO} b_Q\right)^2 + \left(\frac{\partial PVR}{\partial mPa} b_{mPa}\right)^2} \qquad \text{C.7}$$

$$s_{PVR} = \pm\sqrt{\left(\frac{\partial PVR}{\partial CO} s_Q\right)^2 + \left(\frac{\partial PVR}{\partial mPa} s_{mPa}\right)^2} \qquad \text{C.8}$$

where $b_{mPa} = b_{PAP}$ and $s_{mPa} = s_{PAP}$. The uncertainty in the resulting PVR measurement is 0.19 mmHg/Lpm.

The PVC is a function of the cardiac output, the PA pulse pressure (P_d) and the heart rate. The b_{HR} was a bias error of ±0.5 bpm. The calculated uncertainties found using equations C.9 and C.10 for selected points are shown in

$$b_{PVC} = \pm\sqrt{\left(\frac{\partial PVC}{\partial CO} b_Q\right)^2 + \left(\frac{\partial PVC}{\partial \Delta p} b_{Pd}\right)^2 + \left(\frac{\partial PVC}{\partial HR} b_{HR}\right)^2} \qquad \text{C.9}$$

$$s_{PVC} = \pm\sqrt{\left(\frac{\partial PVC}{\partial CO} s_Q\right)^2 + \left(\frac{\partial PVC}{\partial Pd} s_{Pd}\right)^2} \qquad \text{C.10}$$

Table C. 1. Standard systematic uncertainties (b), random uncertainties (s) and 95% confidence interval uncertainties (u) for all global measurements

Measurement	*b*	*s*	*u*
RVP (mmHg)	0.192	0.199	0.541
PAP (mmHg)	0.192	0.204	0.549
P_d (mmHg)	0.192	0.147	0.289
CO (Lpm)	0.050	0.126	0.266
TVG (mmHg)	0.271	0.285	0.771
RF% (32%)	0.006	0.015	0.031
RF%(21%)	0.008	0.020	0.043
PVR (3 mmHg/Lpm)	0.049	0.086	0.194
PVC (2.7 mL/mmHg)	3.80E-05	6.90E-05	1.54E-04

The standard uncertainties of b and s for every measurement are listed in the Table C. 1. The total 95% confidence interval uncertainties in each measurement are also reported.

PIV measurements

The main sources for PIV measurement errors are typically particle size, in-plane loss of particle pairs, seeding density, particle displacement, and background noise [118]. Raffel et al. [118] present results from Monte Carlo simulation work that predict the effect of these contributors. Based on these results and the conditions of the current study (64x64 interrogation window, 5-8 pixel displacement), the uncertainty in the pixel displacement was found using Figures 5.23b, 5.24, 5.27, 5.29, 5.32, and 5.34 published by Raffel et al. [118]. The values used to determine the uncertainty in pixel displacement are shown in Table C. 2.

Table C. 2. PIV measurement error sources and levels (as taken from Raffell et al.[118])

Error Source	Error (pixels)
Particle size (bias)	0.01
In plane loss of pairs (bias)	-0.01
Particle size (rms)	0.05
Pixel displacement (rms)	0.05
Particle image density (rms)	0.04
Noise level of 50%	0.10

The final uncertainty was calculated as ± 0.13 pixels (95% CI) using the RSS method. The uncertainty in the velocity measurements was found using equation C.11.

$$u_{pixel} \text{*pixel calibration/}\Delta t \qquad\qquad\qquad \text{C.11}$$

The pixel calibration is 22.7 µm/pixel and Δt was chosen as 50 µs. This corresponds to an uncertainty in the velocity of ±0.059 m/s.

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