Real time analysis of combustion emissions: a comparison of catalyst treated and untreated solid fuels

Antony Nyombi,¹ Michael R. Williams,² and Roland Wessling,¹

 ¹Cranfield Forensic Institute, Cranfield University – Shrivenham, Defense Academy of the UK, United Kingdom
²Center for Defense Chemistry, Cranfield University – Shrivenham, Defense Academy of the UK, United Kingdom

Abstract

Carbon monoxide (CO) from combustion of solid fuels causes some deaths worldwide every year. This study has been undertaken to evaluate the amount of carbon monoxide, (and carbon dioxide, nitrogen oxide & methane) evolved from catalyst (Pd-Sn/alumina and Cu-Mn/graphite) treated charcoal briquettes, untreated charcoal briquettes, commercial charcoal and coal at non-isothermal temperatures between 50 to 800 °C attained at different heating rates of 20-40 (°C/min). Samples were heated in a thermal analysis instrument coupled with a multi-gas analyser under flowing air at different flow rates 20-100 (ml/min). Results showed a significant CO and NO reduction with catalyst treated charcoal compared to untreated charcoal briquettes and coal. There is also a strong dependence of CO emissions on heating rate and air flow. This study shows that catalyst treatment of solid fuels helps to minimise harmful combustion emissions.



Real time analysis of combustion emissions: a comparison of catalyst treated and untreated solid fuels

Nyombi A^a, Williams R M^b, Wessling R^a

^aCranfield Forensic Institute – Cranfield University, The Defence Academy of the UK – Shrivenham. SN6 8LA ^bCenter for Defence Chemistry – Cranfield University, The Defence Academy of the UK – Shrivenham. SN6 8LA

What is the project about?

Impregnation of Pd-Sn/alumina catalyst on solid fuels has been used as a viable way to minimise toxic combustion emissions while enhancing energy output and combustion efficiency.

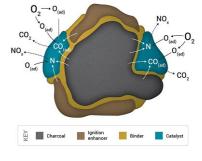
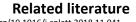


Fig.1: Catalyst treated briquette

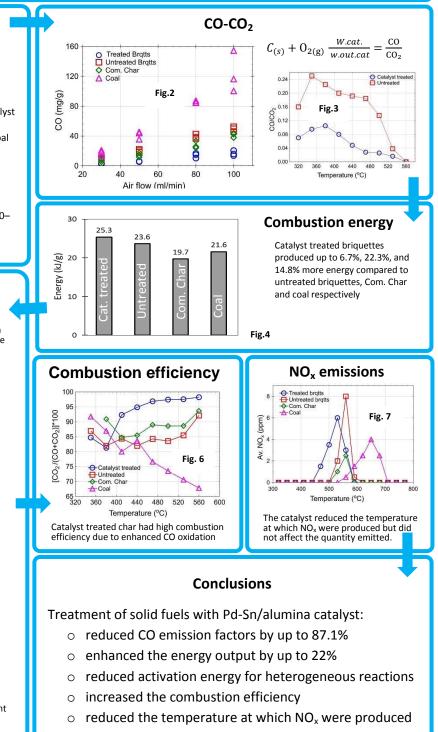
The thermal responses of catalyst treated (Fig.1) and untreated briquettes, commercial charcoal and coal were analysed with TGA/DSC combined with a MultiRae lite gas analyser for combustion products CO. CO₂. NO_x, and CH₄. Samples were heated at 20-40 °C/min and 30-100 ml/min in air (21% O₂)

Kinetics -0.6 α=0.20 α=0.30 α=0.40 Fig.5a: Friedman Plot to determine E_a at different -1.2 α=0.50 -α=0.60 conversions $\ln[\beta_k(d\alpha/dT)_{\alpha,k}]$ α=0.70 $\alpha = 0.80$ -1.8 α=0.90 - α=0.95 -2.4 Friedman plot Ø Ø -3.0 3 1.20 1.26 1.32 1.38 1.44 1.50 1000/T (K⁻¹) 1.0 O 100 ml/min o 80 ml/min Fig. 5b: Scatter 50 ml/min 0.8 plot for E_a Λ 30 ml/min difference Conversion - a (Ecat.td-Euntd) 0.6 0 M 0.4 AD 0 E_{cat.td} - E_{untd} 0.2 A 00 $\Delta \diamond$ 0.0 -100 150 -150 -50 0 50 100 200 250 Energy difference (kJ/mol)

The negative E_a difference at 0.05< α <0.5 for 30 ml/min; 0.2< α <0.9 for 50 ml/min, and $0.5 < \alpha < 0.9$ for 80, and 100 ml/min implied that catalyst treatment lowered the activation energy for char oxidation



- https://doi.org/10.1016/j.cplett.2018.11.041 https://doi.org/10.1080/15567036.2019.1623348 0 0
- 0 0 https://doi.org/10.1007/s40789-018-0229-v
- https://doi.org/10.3389/fchem.2018.00032
- https://doi.org/10.1016/j.catcom.2018.03.011 https://doi.org/10.3390/agriculture5030561 0 0



Future work

- Food safety aspects of catalyst treated solid fuels Environmental friendliness Synthesis of high temp.
- 0 (>600°C) stable catalysts

Acknowledgement



Email: a.nyombi@cranfield.ac.uk, / m.r.williams@cranfield.ac.uk, / r.wessling@cranfield.ac.uk

0