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# **Study of Thermal Convection in Micropolar Fluids Occupying a Rectangular Box**

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# Abstract

This paper is a Fourier-series assisted numerical study of two-dimensional steady thermal convection in micropolar fluid occupying a rectangular box. The horizontal walls of the cavity are uniformly heated to establish a linear temperature in the vertical direction. The vertical walls are insulated. The critical Rayleigh number is obtained numerically as a function of coupling parameter, couple stress parameter and aspect ratio, and the same is plotted graphically. The results of slender vertical, rectangular and square box of finite aspect ratio are obtained as limiting cases of the study.

**Keywords**: Benard convection, critical Rayleigh number, Fourier series, micropolar fluid, aspect ratio.

# 1. Introduction

Convective flow in a thin layer of fluid, free at the upper surface and heated from below, is of fundamental importance and a prototype to a more complex configuration in experiments and industrial processes. The convective flows in a liquid layer can be

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driven by buoyancy forces due to temperature gradients and / or thermo capillary forces caused by surface tension gradients. Thermal convective problems have long been studied extensively since the pioneering experimental and theoretical works of Benard [1], Rayleigh [2] and Pearson [3]. Most of the previous studies were concerned with convection in Newtonian fluids. However, much less work has been done on convection in non-Newtonian fluids such as the micropolar fluids. The theory of micropolar fluids, as developed by Eringen [4], has been a field of sprightly research for the last few decades especially in many industrially important fluids like paints, polymeric suspensions, colloidal fluids, and also in physiological fluids such as normal human blood and snivel fluids. Rama Rao [5] studied the effect of a magnetic field on convection in a micropolar fluid. Sharma and Gupta [6] studied convection in micropolar fluids in a porous medium. Siddheshwar and Sri Krishna [7] presented both linear and nonlinear analyses of convection in a micropolar fluid occupying porous medium. Rudraiah and Siddheshwar [8] analysed the effects of non-uniform temperature gradients of parabolic and stepwise types on the onset of Marangoni convection in a micropolar fluid. This study was later extended by Siddheshwar and Pranesh [9] to include the effect of a magnetic field and buoyancy forces. The effect of non uniform temperature gradient on Benard convection in micropolar fluids, single tem Galerkin expansion technique has been using investigated by Siddheshwar and Pranesh [10]. In this paper, we have investigated the effect of couple stress parameter, coupling parameter and aspect ratio on critical Rayleigh number in a rectangular, square and slender vertical box numerically.

## Nomenclature

Α	Aspect ratio
b	Breadth of rectangular cavity

- 0
- gAcceleration due to gravity
- *h* Height of rectangular cavity
- *I* Momentum of Inertia

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、 、	
$\vec{\omega}$	Spin
$N_1$	Coupling parameter
$N_2$	Inertia parameter
$N_3$	Couple stress parameter
р	pressure
Pr	Prandtl number
$\rightarrow$	
q	Velocity
Ra	Rayleigh number
Rac	Critical Rayleigh number
и	Horizontal velocity component
w	Vertical velocity component
x	Horizontal Cartesian coordinate
Z	Vertical Cartesian coordinate

# **Greek symbols**

- $\alpha$  Co-efficient of thermal expansion
- $\Delta T$  Temperature difference between the two horizontal plates
- $\chi$  Thermal diffusivity
- $\eta$  Co-efficient of shear kinematic viscosity
- $\eta'$  Co-efficient of spin viscosity
- $\lambda'$  Co-efficient of bulk viscosity
- $\psi$  Stream function
- $\rho$  Actual density
- $\rho_0$  Reference density
- $\theta$  Deviation from static temperature
- $\zeta$  Co-efficient of coupling viscosity or vortex viscosity

 $\nabla$  Differential operator

 $\nabla^2_A$  Modified Laplacian operator

## Subscripts

*c* Critical quantity

## Superscripts

\* Dimensionless quantity

# 2. Mathematical Formulation

We consider two-dimensional thermal convection in micropolar fluids occupying a rectangular box with height *h* and width *b*. We choose a cartesian coordinate system with the *x*-axis in the horizontal direction and *z*-axis in the vertical direction. The horizontal walls are at z = 0 and z = h and the vertical walls are at  $x = -\frac{b}{2}$  and  $x = \frac{b}{2}$  as shown in Fig. 1. The fluid is heated from below and cooled from above as in a typical Rayleigh-Benard problem, the temperature difference between the bounding walls being  $\Delta T$ .



Figure 1: Schematic diagram of the flow configuration.

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The governing equations are:

# **Continuity equation:**

$$\overrightarrow{\nabla \cdot q} = 0 \tag{1}$$

## Conservation of linear momentum:

$$\rho_0 \left[ \begin{pmatrix} \rightarrow \\ q \cdot \nabla \end{pmatrix} \stackrel{\rightarrow}{q} \right] = -\nabla p + \rho g + (2\zeta + \eta) \nabla^2 \stackrel{\rightarrow}{q} + \zeta \begin{pmatrix} \rightarrow \\ \nabla \times \omega \end{pmatrix}$$
(2)

## Conservation of angular momentum:

$$\rho_0 I\left[\begin{pmatrix} \overrightarrow{q} \cdot \nabla \\ \overrightarrow{q} \cdot \nabla \\ \overrightarrow{\omega} \end{bmatrix} = (\lambda' + \eta') \nabla\left(\nabla \cdot \overrightarrow{\omega}\right) + \eta' \nabla^2 \overrightarrow{\omega} + \zeta\left(\nabla \times \overrightarrow{q}\right) - 2\zeta \overrightarrow{\omega}$$
(3)

**Conservation of energy:** 

$$\begin{pmatrix} \rightarrow \\ q \cdot \nabla \end{pmatrix} T = \chi \nabla^2 T \tag{4}$$

## **Equation of State:**

$$\rho = \rho_0 \left( 1 - \alpha \left( T - T_0 \right) \right). \tag{5}$$

In the Micropolar fluid, the particle spin matches with the vorticity of the carrier fluid and this result in an additional biharmonic term in equation (2). This is a drag term contributed to by the suspended particles. The effect of suspended particles in equation (4) on

temperature *T* comes through the velocity *q*. The upper and lower boundaries are at isothermal temperatures  $T_0$  and  $T_0 + \Delta T$  respectively, where  $\Delta T$  is positive temperature difference. All the boundaries are assumed to be impermeable and perfectly heat conducting. From the governing equations (1) – (5) it follows that a motionless conduction state exists only if the static temperature distribution is independent of *x* and depends linearly on *z*. The present study is restricted to this case.

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It is convenient to express the temperature in the form

$$T = T_0 + \varDelta T \left( 1 - \frac{z}{h} \right) + \theta \tag{6}$$

where  $\theta$  is the deviation from the static temperature. The component forms of equations (1) - (5) for steady flow are:

$$\frac{\partial u}{\partial x} + \frac{\partial w}{\partial z} = 0 , \qquad (7)$$

$$\frac{1}{\rho_o}\frac{\partial p}{\partial x} - \frac{(2\zeta + \eta)}{\rho_0} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial z^2}\right) + \frac{\zeta}{\rho_0}\frac{\partial \omega_y}{\partial z} + u\frac{\partial u}{\partial x} + w\frac{\partial u}{\partial z} = 0, \quad (8)$$

$$\frac{1}{\rho_o}\frac{\partial p}{\partial z} - \frac{(2\zeta + \eta)}{\rho_0} \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial z^2}\right) - \frac{\zeta}{\rho_0}\frac{\partial \omega_y}{\partial x} + \frac{\rho}{\rho_0}g + u\frac{\partial w}{\partial x} + w\frac{\partial w}{\partial z} = 0$$
(9)

$$\eta' \left( \frac{\partial^2 \omega_y}{\partial x^2} + \frac{\partial^2 \omega_y}{\partial z^2} \right) + \zeta \left( \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \right) - 2\zeta \omega_y - \rho I \left( u \frac{\partial \omega_y}{\partial x} + w \frac{\partial \omega_y}{\partial z} \right) = 0 \quad (10)$$

$$\chi \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial z^2} \right) - u \frac{\partial T}{\partial x} - w \frac{\partial T}{\partial z} = 0$$
(11)

$$\rho = \rho_o \left[ 1 - \alpha \, \varDelta T \left( 1 - \frac{z}{h} \right) - \alpha \, \theta \right]. \tag{12}$$

Since the flow is two-dimensional, we introduce the stream function  $\psi$  by

$$u = \frac{\partial \psi}{\partial z}, \quad w = -\frac{\partial \psi}{\partial x}.$$
 (13)

We also define non-dimensional variables denoted by asterisks

$$(x^*, z^*) = \left(\frac{x}{b}, \frac{z}{h}\right), \ T^* = \frac{T}{\Delta T}, \ \omega_y^* = \frac{h^2}{\chi} \omega_y, \ \theta^* = \frac{\theta}{\Delta T}, \ \psi^* = \frac{\psi}{\chi}.$$
(14)

By eliminating the pressure from (8) and (9), introducing the expressions (13) and (14) into the resulting equation and equation (10) and (11) and dropping the asterisk, we get the governing equations in the following form:

$$(1+N_1)\nabla_A^2\psi - A^4Ra\frac{\partial\theta}{\partial x} - N_1\nabla_A^2\omega_y + \frac{A}{\Pr}\frac{\partial(\psi,\nabla_A^2\psi)}{\partial(x,z)} = 0, \qquad (15)$$

$$N_{3}\nabla_{A}^{2}\omega_{y} + A^{2}N_{1}\nabla_{A}^{2}\psi - 2A^{2}N_{1}\omega_{y} + \frac{AN_{2}}{\Pr}\frac{\partial(\psi,\omega_{y})}{\partial(x,z)} = 0 , \qquad (16)$$

$$A^{2}\frac{\partial\psi}{\partial x} - A\nabla_{A}^{2}\theta - A^{2}\frac{\partial(\psi,\theta)}{\partial(x,z)} = 0, \qquad (17)$$

where

$$A = \frac{h}{b}, \ \nabla_A^2 = A^2 \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial z^2}, \ N_1 = \frac{\zeta}{\zeta + \eta}, \ N_2 = \frac{I}{b^2},$$
$$N_3 = \frac{\eta'}{(\zeta + \eta)b^2}, \ \Pr = \frac{\rho_0 \psi}{\zeta + \eta}, \ Ra = \frac{\rho_0 \alpha g \, \Delta T b^3}{\chi(\zeta + \eta)}$$

and boundary conditions are

$$\psi = \nabla_A^2 \psi = \theta = \omega_y = 0 \text{ at } \begin{cases} x = -\frac{1}{2}, & x = \frac{1}{2}, & 0 < z < 1 \\ z = 0, & z = 1, & -\frac{1}{2} < x < \frac{1}{2} \end{cases}$$
(18)

## 3. Linear Stability

The onset of thermal convection is described by the linear versions of equations (15), (16) and (17). To make this study we neglect the Jacobians in equations (15), (16) and (17) leads to

$$(1+N_1)\nabla_A^2 \psi - A^4 Ra \frac{\partial \theta}{\partial x} - N_1 \nabla_A^2 \omega_y = 0, \qquad (19)$$

$$A^{2}N_{1}\nabla_{A}^{2}\psi + \left(N_{3}\nabla_{A}^{2} - 2A^{2}N_{1}\right)\omega_{y} = 0, \qquad (20)$$

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$$\nabla_A^2 \theta - A \frac{\partial \psi}{\partial x} = 0.$$
 (21)

By eliminating  $\omega_y$  between (19) and (20) leads us to differential equation of sixth order as

$$(1+N_1)N_3\nabla_A^6\psi - A^2(2+N_1)N_1\nabla_A^4\psi + 2N_1A^6Ra\frac{\partial\theta}{\partial x}$$

$$-A^4N_3Ra\left(A^2\frac{\partial^3\theta}{\partial x^3} + \frac{\partial^3\theta}{\partial x\partial z^2}\right) = 0.$$
(22)

The solutions of (21) and (22) can be expanded in the half range Fourier sine series:

$$\psi = \sum_{n=1}^{\infty} C_n(x) \sin n\pi z$$
(23)

$$\theta = \sum_{n=1}^{\infty} F_n(x) \sin n\pi z$$
(24)

Equations (21) and (22) are solved for stress free, isothermal boundaries, hence we have the boundary conditions in terms of  $C_n(x)$  and  $F_n(x)$  are:

$$C_n(x) = \frac{d^2}{dx^2} [C_n(x)] = \frac{d^4}{dx^4} [C_n(x)] = F_n(x) = 0 \text{ at } x = \pm \frac{1}{2}$$
(25)

Using (23) and (24) with the boundary condition (25) into the linearized versions of the governing equations (21) and (22), and equating coefficients of  $\sin n\pi z$ , leads to set of ordinary differential equations

$$\left(A^{2}\frac{d^{2}}{dx^{2}} - n^{2}\pi^{2}\right)F_{n} - A\frac{dC_{n}}{dx} = 0$$
(26)

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$$A^{6}[(1+N_{1})N_{3}]\frac{d^{6}C_{n}}{dx^{6}} - A^{4}\left[3n^{2}\pi^{2}(1+N_{1})N_{3} + A^{2}(2+N_{1})N_{1}\right]\frac{d^{4}C_{n}}{dx^{4}} + A^{2}\left[3n^{4}\pi^{4}(1+N_{1})N_{3} + 2n^{2}\pi^{2}A^{2}(2+N_{1})N_{1}\right]\frac{d^{2}C_{n}}{dx^{2}} - \left[n^{6}\pi^{6}(1+N_{1})N_{3} + n^{4}\pi^{4}A^{2}(2+N_{1})N_{1}\right]C_{n} + A^{4}\left[2N_{1}A^{2}Ra\frac{d}{dx} + n^{2}\pi^{2}N_{3}Ra\frac{d}{dx} - N_{3}A^{2}Ra\frac{d^{3}}{dx^{3}}\right]F_{n} = 0.$$

$$(27)$$

By eliminating  $F_n$  between (26) and (27) leads us to an ordinary differential equation of eighth order in  $C_n$  as

$$A^{8} [(1+N_{1})N_{3}] \frac{d^{8}C_{n}}{dx^{8}} - A^{6} \Big[ 4n^{2}\pi^{2}(1+N_{1})N_{3} + A^{2}(2+N_{1})N_{1} \Big] \frac{d^{6}C_{n}}{dx^{6}} + A^{4} \Big[ 3n^{2}\pi^{2}A^{2}(2+N_{1})N_{1} + 6n^{4}\pi^{4}(1+N_{1})N_{3} - N_{3}A^{3}Ra \Big] \frac{d^{4}C_{n}}{dx^{4}} - A^{2} \Big[ 4n^{6}\pi^{6}(1+N_{1})N_{3} + 3n^{4}\pi^{4}A^{2}(2+N_{1})N_{1} \Big] \frac{d^{2}C_{n}}{dx^{2}} + \Big[ n^{8}\pi^{8}(1+N_{1})N_{3} + n^{6}\pi^{6}A^{2}(2+N_{1})N_{1} \Big] C_{n} = 0, \qquad (28)$$

with boundary conditions

$$C_n\left(\pm\frac{1}{2}\right) = \frac{dC_n}{dx}\left(\pm\frac{1}{2}\right) = \frac{d^2C_n}{dx^2}\left(\pm\frac{1}{2}\right) = \frac{d^4C_n}{dx^4}\left(\pm\frac{1}{2}\right) = 0.$$
 (29)

The general solution of differential equation (28) for n = 1 is

$$C_{1}(x) = a_{1}e^{m_{1}x} + a_{2}e^{m_{2}x} + a_{3}e^{m_{3}x} + a_{4}e^{m_{4}x} + a_{5}e^{m_{5}x} + a_{6}e^{m_{6}x} + a_{7}e^{m_{7}x} + a_{8}e^{m_{8}x}$$
(30)

where  $a_i$ 's are arbitrary constants and  $m_i$ 's are roots of the auxiliary equation of (28) with  $m_2 = -m_1$ ,  $m_4 = -m_3$ ,  $m_6 = -m_5$ ,  $m_8 = -m_7$ .

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Equations (29) and (30) give us eight homogenous equations in the eight unknowns  $a_1$ ,  $a_2$ ,  $a_3$ ,  $a_4$ ,  $a_5$ ,  $a_6$ ,  $a_7$ ,  $a_8$ . For a non-trivial solution for the system we require

$$\begin{vmatrix} e^{0.5m_{1}} & e^{-0.5m_{1}} & e^{0.5m_{3}} & e^{-0.5m_{3}} & e^{0.5m_{3}} & e^{-0.5m_{3}} & e^{0.5m_{3}} & e^{-0.5m_{3}} & e^{0.5m_{3}} & e^{-0.5m_{3}} \\ e^{-0.5m_{1}} & e^{0.5m_{1}} & e^{-0.5m_{3}} & e^{0.5m_{3}} & e^{-0.5m_{3}} & e^{0.5m_{3}} & e^{-0.5m_{3}} & e^{0.5m_{3}} \\ m_{1}e^{0.5m_{1}} & -m_{1}e^{-0.5m_{1}} & m_{3}e^{0.5m_{3}} & -m_{3}e^{-0.5m_{3}} & m_{5}e^{-0.5m_{3}} & m_{7}e^{-0.5m_{3}} & -m_{7}e^{-0.5m_{3}} \\ m_{1}e^{-0.5m_{1}} & -m_{1}e^{0.5m_{1}} & m_{3}e^{-0.5m_{3}} & -m_{3}e^{0.5m_{3}} & m_{5}e^{-0.5m_{3}} & m_{7}e^{-0.5m_{3}} & -m_{7}e^{-0.5m_{3}} \\ m_{1}^{2}e^{-0.5m_{1}} & m_{1}^{2}e^{-0.5m_{1}} & m_{3}^{2}e^{-0.5m_{3}} & m_{5}^{2}e^{-0.5m_{3}} & m_{5}^{2}e^{-0.5m_{3}} & m_{7}^{2}e^{-0.5m_{3}} & m_{7}^{2}e^{-0.5m_{3}} \\ m_{1}^{2}e^{-0.5m_{1}} & m_{1}^{2}e^{-0.5m_{1}} & m_{3}^{2}e^{-0.5m_{3}} & m_{5}^{2}e^{-0.5m_{3}} & m_{5}^{2}e^{-0.5m_{3}} & m_{7}^{2}e^{-0.5m_{3}} & m_{7}^{2}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{3}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{5}^{4}e^{-0.5m_{3}} & m_{7}^{4}e^{-0.5m_{3}} \\ m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m_{1}} & m_{1}^{4}e^{-0.5m$$

The left hand side of (31) may be viewed as a function  $Ra_c$ , say  $f(Ra_c)$ , with  $Ra_c$  depending on A,  $N_1$  and  $N_3$ , hence equation (31) can be written as  $f(Ra_c) = 0$ . Using Newton–Raphson method for various values of A,  $N_1$  and  $N_3$ ,  $Ra_c$  can be calculated numerically, using the iterative formula

$$(Ra_{c})_{k+1} = (Ra_{c})_{k} - \frac{f((Ra_{c})_{k})}{f'((Ra_{c})_{k})}$$
(32)

where prime denotes differential of  $f(Ra_c)$  with respect to  $Ra_c$  and the paper calculation based on Newton-Raphson method were done using Matlab.

#### 4. Results and Discussion

The thermal convection in micropolar fluids occupying a rectangular box is investigated numerically using linear stability theory assisted by Fourier series. Different aspect ratios are considered to cover the results of slender, square and rectangular cavity. In the present paper, the behavior of the system as a function of the critical Rayleigh number,  $Ra_c$ , depends upon the aspect ratio *A*, coupling parameter  $N_1$  and couple stress parameter  $N_3$ . For fixed  $N_3$ , the variation of  $Ra_c$  for steady thermal convection with  $N_1$  for different values of *A* is shown in figure 2. From this we observe that the  $Ra_c$  increases with increases with  $N_1$  and decreases 138

with increase in the value of *A*. From the plot of  $Ra_c^*$  [ $Ra_c^* = Ra_c - Ra_c$  (at  $N_3 = 1$ )] versus  $N_3$  for different  $N_1$  in a rectangular, square and vertical slender box, we observe that  $Ra_c^*$  increases with increase in  $N_1$  and  $N_3$  and decreases with increase in *A* as shown in figure 3. In the absence of coupling parameter, i.e., for  $N_1 = 0$ , the value of  $Ra_c = 657.51$  (classical Rayleigh-Benard result) is obtained for a square box (A = 1) and for  $N_3 \neq 0$ .



Figure 2: Plot of critical  $Ra_c$  versus A, for different values of N1 and for N3 = 1.0, for A < 1(shallow box), A = 1 (square box) and A > 1 (slender vertical box).



Figure 3: Plot of  $Ra_c^*$  versus  $N_3$ , for a various values of  $N_1$  and A.

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# References

[1] H Benard, Les tourbillons cellulaires dans une nappe liquide, *Revue Generale des Sciences pures et Appliquees*, vol. 11, pp. 1261-1271, 1990.

[2] L Rayleigh, On convection currents in a horizontal layer of fluid when the higher temperature is on the other side, *Philosophical Magazine*, vol. 32, pp. 529–546, 1916.

[3] J R A Pearson, On convection cells induced by surface tension, *J. Fluid Mech.*, vol. 4, pp. 489–500, 1958.

[4] A C Eringen, Micropolar theory of liquid crystals: *In: Liquid Crystals and Ordered Fluids* (J F Johnson and R S Porter, Eds.), vol. 3, Plenum Publishing, New York, 1978.

[5] K V Rama Rao, Thermal instability in a micropolar fluid layer subject to a magnetic field, *Int. J. Engng.* Sci., vol. 18, pp. 741-750, 1980.

[6] R C Sharma and U Gupta, Thermal convection in Micropolar fluids in porous medium, *Int. J. Engng.* Sci., vol. 33, pp. 1887-1892, 1995.

[7] P G Siddheshwar and C V Sri Krishna, Linear and non-linear analyses of convection in a Micropolar fluid occupying a porous medium, *Int. J. Non-linear Mech.*, vol. 38, pp. 561-579, 2003.

[8] N Rudraiah and P G Siddheshwar, Effect of non-uniform basic temperature gradient on the onset of Marangoni convection in a fluid with suspended particles, *Aerospace Science and Tech.*, vol. 4, pp. 517-523, 2000.

[9] P G Siddheshwar and S Pranesh, Magneto convection in fluids with suspended particles under lg and g, *Aerospace Science and Tech.*, vol. 6, pp. 105-114, 2002.

[10] P G Siddheshwar and S Pranesh, Effect of a non-uniform basic temperature gradient on Rayleigh-Benard convection in a micropolar fluid, *Int. J. Engg., Sci.*, vol. 36, pp. 1183–1196, 1998.