



Article

A PDE-Based Data Reconciliation Approach for Systems with Variations of Parameters

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Abstract. Data reconciliation is a mathematical approach that improves the quality of measurements by calculating the reconciled data that satisfy the process constraints. The conventional data reconciliation approach relies on the process model that contains the constant parameters. In the industrial applications, however, there are always possible variations of parameters within the system. In this paper, a new data reconciliation approach based on the partial differential equation (PDE) is developed. The proposed data reconciliation approach is experimentally applied to a case study of temperature measurements for a refinery process. The PDE-based model is employed in the formulation of the optimization problem. Unlike the conventional data reconciliation approach in which the system is assumed to be lumped, the PDE-based data reconciliation approach includes in the problem formulation the variations of parameters within the system in order to describe the real system's behaviour. The reconciled values can be computed within the computational domain so they can be used as the data for troubleshooting, equipment analysis and maintenance.

Keywords: Data reconciliation, partial differential equation, variations of parameters, temperature measurements.

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1. Introduction

Chemical processes are usually involved with the technologies that change some reactants into more useful products. In the real operations of chemical processes, the process variables must be measured for monitoring and control at the profitable conditions. The measurement values, however, inevitably contain errors at some certain levels. Thus, a data pre-processing technique is important in the industrial operations. Data reconciliation is one of the techniques extensively used in order to improve the quality of measurements [1-3].

In the conventional data reconciliation approach, the reconciled data can be obtained by solving the optimization problem which minimizes the measurement errors subject to some process constraints [4, 5]. The models based on mass and energy balances are usually employed in order to describe the system behaviour. Plácido et al. [6] applied the data reconciliation approach to a petroleum refinery process in order to detect the unexpected flow deviation and product loss. The quality of the measured data was improved due to the fact that the effects of random and gross errors were reduced. Sarabia et al. [7] applied the data reconciliation approach to the optimal management of hydrogen network in a petrol refinery. The reconciled data strictly satisfied a set of mass balance equations employed in the formulation of the optimization problem. In Nguyen et al. [8], a model of an upstream petroleum plant was developed based on the reconciled data of material and energy streams. The process model employed in the data reconciliation was based on the conservation of mass and energy. In Özyurt and Pike [21], the simultaneous data reconciliation and gross error detection methods were applied to the chemical processes. The quality of the measured data was improved by calculating the reconciled data satisfying the process models. Although the effects of random and gross errors in the measurements are reduced, the conventional data reconciliation approach employs the models with no variations of parameters. For the systems with the variations of parameters, however, a more advanced modeling approach should be developed and included in the formulation of the data reconciliation problem.

Due to some advances in the computational techniques, the partial differential equation (PDE) can be developed to describe the system behaviour within the computational domain. The PDE-based model can be used to predict the values of some variables such as temperature, concentration and so on [9-14] at different positions within the system. Haghshenasfard and Hooman [15] used the PDE to predict the rate of asphaltene deposition from crude oil. It was found that the rate of asphaltene deposition depended on various operating parameters such as temperature, Reynolds number and asphaltene concentration. Bayat et al. [16] predicted the fouling behaviour in an industrial shell and tube heat exchanger. The contours of coke concentration and velocity profile were calculated. Alshammari and Hellgardt [17] performed an analysis for hydrothermal conversion of heavy oil in a continuous flow reactor. The effects of radial mass transport were taken into account using the PDE. The temperature, concentration and velocity profiles in the reactor were computed. Rukthong et al. [18] performed the computational fluid dynamics (CFD) simulation of a pipeline for the crude oil transport. The effects of crude oil properties on the transport profiles were studied.

The variations of parameters usually occur within the system in practice [18-20], e.g., variations of physical and chemical properties within the system. In this paper, the PDE-based model is employed in the formulation of the data reconciliation problem. Unlike the conventional data reconciliation approach [21] in which the models with constant parameters are considered, the PDE-based data reconciliation approach includes in the problem formulation the variations of parameters within the system in order to describe the behaviour of the real system.

The paper is organized as follows. The experimental setup is presented in Section 2. Section 3 describes the modeling equations. The boundary conditions are described in Section 4. The optimization problem formulation is presented in Section 5. The results and discussions are presented in Section 6. Finally, the paper is concluded in Section 7.

2. Experimental Setup

The PDE-based data reconciliation approach is experimentally applied to a case study of temperature measurements for a refinery process as shown in Fig. 1.

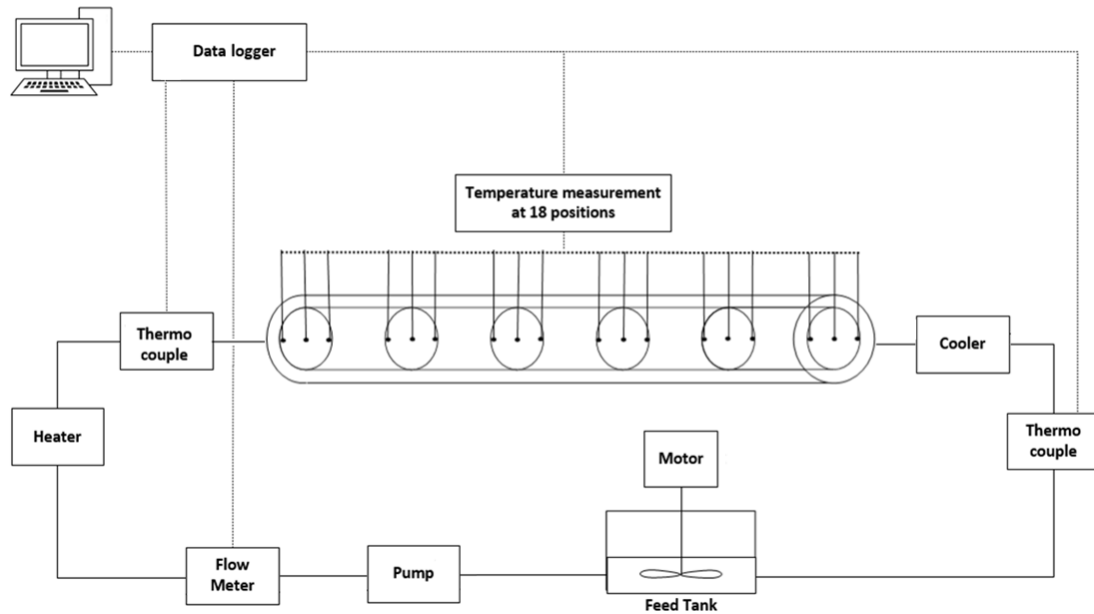


Fig. 1. Flowchart of the experimental setup.

In the experimental setup, the crude oil obtained from an oil refinery in Thailand is contained in a 1 m³ feed tank equipped with a stirrer. The crude oil is supplied to a horizontal pipe for temperature measurements using a feed pump. The pipe length is 3 m and the inner pipe diameter is 0.3 m. At the inlet, the temperature is increased to 330 K using a heater. The values of temperature at 18 measurement positions are measured as shown in Fig. 2.

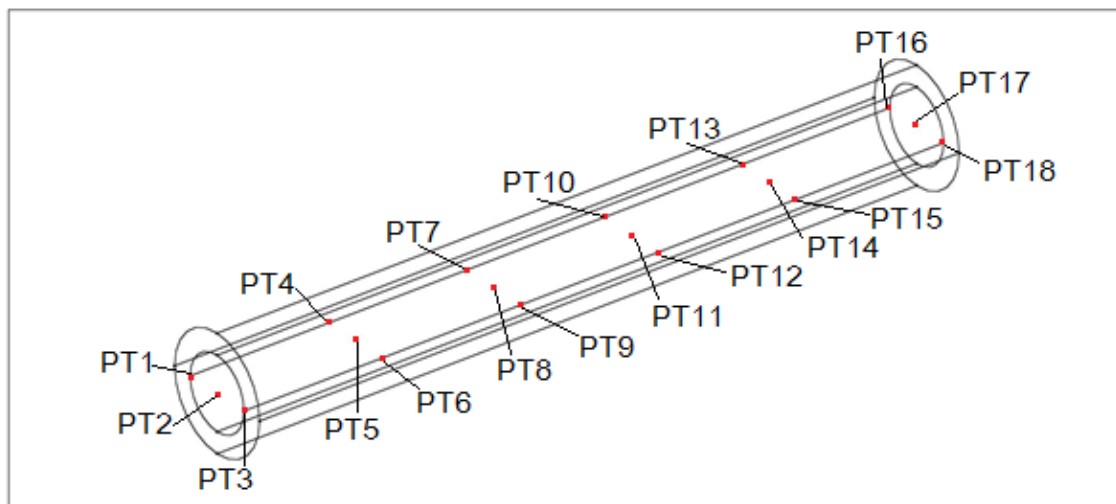


Fig. 2. Horizontal pipe with 18 measurement positions (PT1-PT18).

The system is operated for 10 minutes before the steady-state values of temperature are collected. At the outlet, the temperature is reduced to 303 K using a cooler. The values of the measured temperature are collected using a data logger. The data reconciliation is performed using a computer. The modeling equations are developed and solved in COMSOL Multiphysics 3.5a using the optimization module [23].

3. Modeling Equations

The flow is in the turbulent regime. The flow behaviour can be described by the following Reynolds-Averaged Navier-Stokes (RANS) equations [24, 25]

$$\rho \frac{\partial \mathbf{u}}{\partial t} + \rho \mathbf{u} \cdot \nabla \mathbf{u} = \nabla \cdot [-p\mathbf{I} + (\eta + \eta_T)(\nabla \mathbf{u} + (\nabla \mathbf{u})^T)] + \mathbf{F} \quad (1)$$

$$\nabla \cdot \mathbf{u} = 0 \quad (2)$$

where ρ is the density, \mathbf{u} is the velocity vector, p is the pressure, η is the dynamic viscosity and \mathbf{F} is the body force vector. The turbulent viscosity η_T can be calculated from $\eta_T = \rho C_\mu \frac{k^2}{\varepsilon}$ where k is the turbulent kinetic energy, ε is the turbulent dissipation rate and $C_\mu = 0.09$. The $k-\varepsilon$ turbulence model can be described by

$$\rho \frac{\partial k}{\partial t} - \nabla \cdot \left[\left(\eta + \frac{\eta_T}{\sigma_k} \right) \nabla k \right] + \rho \mathbf{u} \cdot \nabla k = \frac{1}{2} \eta_T (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)^2 - \rho \varepsilon \quad (3)$$

$$\rho \frac{\partial \varepsilon}{\partial t} - \nabla \cdot \left[\left(\eta + \frac{\eta_T}{\sigma_\varepsilon} \right) \nabla \varepsilon \right] + \rho \mathbf{u} \cdot \nabla \varepsilon = \frac{1}{2} C_{\varepsilon 1} \frac{\varepsilon}{k} \eta_T (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)^2 - \rho C_{\varepsilon 2} \frac{\varepsilon^2}{k} \quad (4)$$

where $\sigma_k = 1.0$, $\sigma_\varepsilon = 1.3$, $C_{\varepsilon 1} = 1.44$ and $C_{\varepsilon 2} = 1.92$. The values of the model constants are obtained by comprehensive data fitting for a wide range of turbulent flows [24, 25]. The energy balance consists of the convection and conduction which can be expressed as

$$\rho C_p \left(\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T \right) = \nabla \cdot (\lambda \nabla T) \quad (5)$$

where C_p is the specific heat capacity, T is the temperature and λ is the coefficient of heat conductivity. The modeling equations can be summarized in Table 1.

Table 1. Modeling equations.

Types	Modeling equations
Reynolds-Averaged Navier-Stokes equations	$\rho \frac{\partial \mathbf{u}}{\partial t} + \rho (\mathbf{u} \cdot \nabla) \mathbf{u} = \nabla \cdot [-p\mathbf{I} + (\eta + \eta_T)(\nabla \mathbf{u} + (\nabla \mathbf{u})^T)] + \mathbf{F}$ $\nabla \cdot \mathbf{u} = 0$
$k-\varepsilon$ turbulence model	$\rho \frac{\partial k}{\partial t} - \nabla \cdot \left[\left(\eta + \frac{\eta_T}{\sigma_k} \right) \nabla k \right] + \rho \mathbf{u} \cdot \nabla k = \frac{1}{2} \eta_T (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)^2 - \rho \varepsilon$ $\rho \frac{\partial \varepsilon}{\partial t} - \nabla \cdot \left[\left(\eta + \frac{\eta_T}{\sigma_\varepsilon} \right) \nabla \varepsilon \right] + \rho \mathbf{u} \cdot \nabla \varepsilon = \frac{1}{2} C_{\varepsilon 1} \frac{\varepsilon}{k} \eta_T (\nabla \mathbf{u} + (\nabla \mathbf{u})^T)^2 - \rho C_{\varepsilon 2} \frac{\varepsilon^2}{k}$
Energy balance equation	$\rho C_p \left(\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T \right) = \nabla \cdot (\lambda \nabla T)$

The variations of parameters usually occur within the system in practice, e.g., variations of physical and chemical properties within the system. The PDE-based data reconciliation approach includes in the problem formulation the variations of parameters within the system in order to describe the real system's behaviour. In this paper, the parameters for the flow behaviour and heat transfer as shown in Table 2 are allowed to vary with the temperature [26] at each position within the system.

Table 2. Variations of parameters.

Physical properties	Values
Density (kg/m ³)	$\rho = 840 - 0.59(T - 20)$
Specific heat capacity (J/kg °C)	$C_p = 309614114 - 5.66875T - 0.322T^2$
Dynamic viscosity (Pa.s)	$\eta = 19.54674 - 1.36857(T - 38) + 0.07271(T - 38)^2 - 0.00163(T - 38)^3$
Coefficient of heat conductivity (W/m °C)	$\lambda = 0.16276(1 - 0.00054T)$

4. Boundary Conditions

For the Reynolds-Averaged Navier-Stokes (RANS) equations, the velocity is 4.85 m/s at the inlet. At the outlet, a Dirichlet condition on the pressure is specified as

$$\hat{p} = \hat{p}_o \quad (6)$$

where \hat{p}_o is the reference pressure. For the $k - \varepsilon$ turbulence model, the values of k and ε at the inlet can be calculated from

$$k = \frac{3}{2}(|\mathbf{u}|I_T)^2 \text{ and } \varepsilon = C_\mu^{3/4} \frac{k^{3/2}}{L_T} \quad (7)$$

where I_T is the turbulence intensity and L_T is the turbulent length scale. The value of turbulence intensity I_T is 0.05 for the fully turbulent flow. The turbulent length scale L_T is a measure of the size of eddies that are not solved. For the fully developed flow in pipe, the value of turbulent length scale L_T equals $0.07L$ where L is the inner pipe diameter. At the outlet, the following convective flux conditions are specified for the turbulence variables

$$\mathbf{n} \cdot \nabla k = 0 \text{ and } \mathbf{n} \cdot \nabla \varepsilon = 0 \quad (8)$$

where \mathbf{n} is the normal vector. The logarithmic wall function [25] is applied to the wall. For the energy balance equations, the temperature at the inlet is 330 K. At the outlet, the heat flux vector \mathbf{q} across the boundary is due to convection as

$$\mathbf{q} \cdot \mathbf{n} = \rho C_p T \mathbf{u} \cdot \mathbf{n} \quad (9)$$

This boundary condition is a useful condition in the convection-dominated energy balance. The boundary conditions can be summarized in Table 3.

Table 3. Boundary conditions.

Types	Inlet	Outlet
Reynolds-Averaged Navier-Stokes equations	4.85 m/s	$p = p_o$
$k - \varepsilon$ turbulence model	$k = \frac{3}{2}(u L_T)^2$ $\varepsilon = C_\mu^{3/4} \frac{k^{3/2}}{L_T}$	$n \cdot \nabla k = 0$ $n \cdot \nabla \varepsilon = 0$
Energy balance equation	330.00 K	$q \cdot n = \rho C_p T u \cdot n$

5. Optimization Problem Formulation

In the experiments, the values of temperature are measured at 18 measurement positions as shown in Fig. 2. After the values of temperature have reached the steady state, 100 data sets of the measured temperature $T_{ij,measured}$ are collected where the subscript i denotes the measurement position and j denotes the data set. The objective function of the optimization problem is the following least-squares minimization between the measured temperature $T_{ij,measured}$ and the reconciled temperature $T_{i,reconciled}$

$$\text{minimizing } \sum_{i=1}^N \sum_{j=1}^M \left(\frac{T_{ij,measured} - T_{i,reconciled}}{\sigma_i} \right)^2 \quad (10)$$

where σ_i is the standard deviation at each measurement position i , $N=18$ is the number of measurement positions and $M=100$ is the number of data sets. The objective function (10) is solved subject to the following constraints; (i) modeling equations in Table 1, (ii) variations of parameters in Table 2, (iii) boundary conditions in Table 3 and (iv) constraints on the minimum and maximum values of the reconciled temperature $T_{i,reconciled}$. The PDE-based data reconciliation approach is solved in COMSOL Multiphysics 3.5a using the optimization module. The details on solving the optimization algorithm can be found in [22, 23]. All of the computations have been performed using Intel Core i3, 2.20 GHz and 4GB RAM.

6. Results and Discussions

6.1. Mesh Sensitivity Analysis and Model Validation

In this section, the mesh sensitivity analysis and the model validation are presented. The mesh sensitivity analysis is shown in Fig. 3. For a proper simulation setup, the simulation quality should not be affected by further increasing the number of mesh elements.

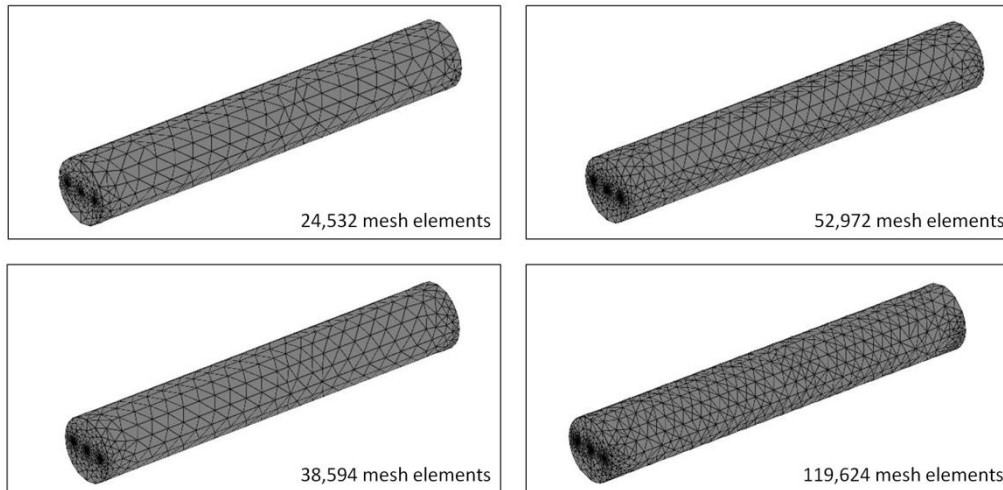


Fig. 3. Mesh sensitivity analysis.

Figure 4 shows the simulation temperature at different positions on the centerline. The simulation results are nearly similar as the number of mesh elements is increased from 52,972 to 119,624 so the number of mesh elements 52,972 is selected in this case.

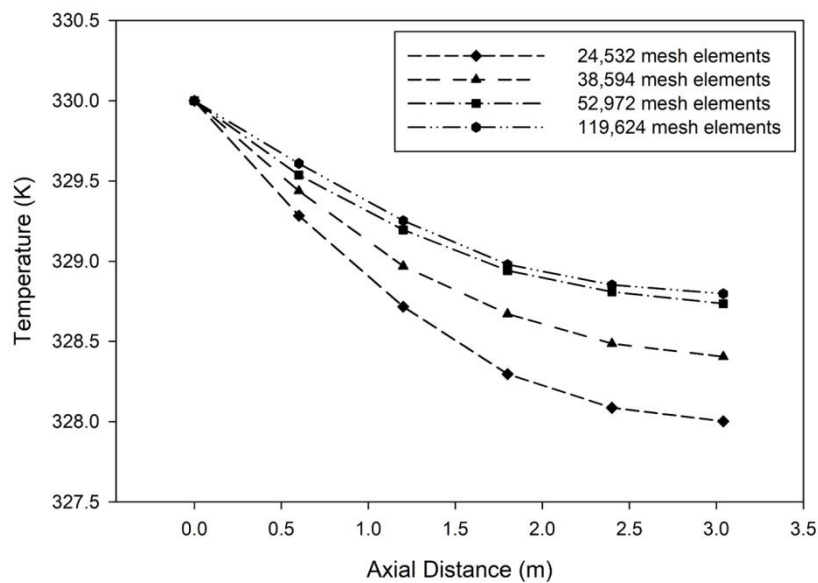


Fig. 4. Simulation temperature at different positions on the centerline.

The model validation is performed by comparing the simulation results with the experimental data obtained from the calibrated thermocouple as shown in Fig. 5. The values of the simulation temperature at different positions on the centerline are in good agreement with those of the experimental data so the developed model can be used for further simulations.

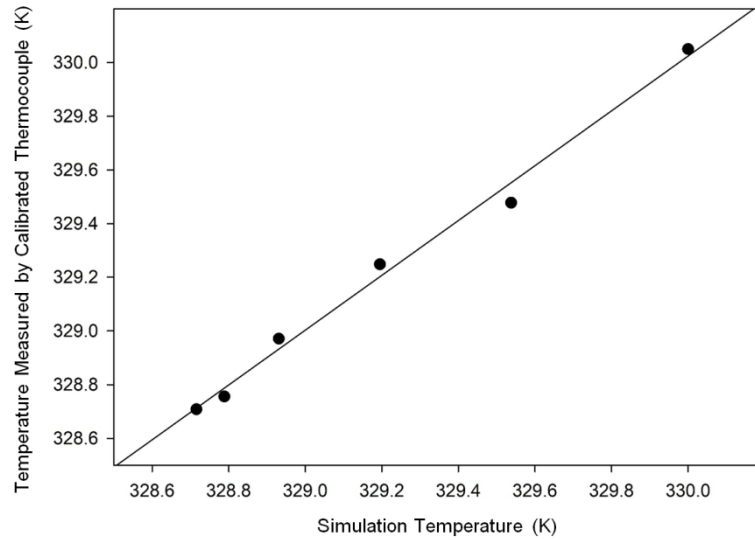
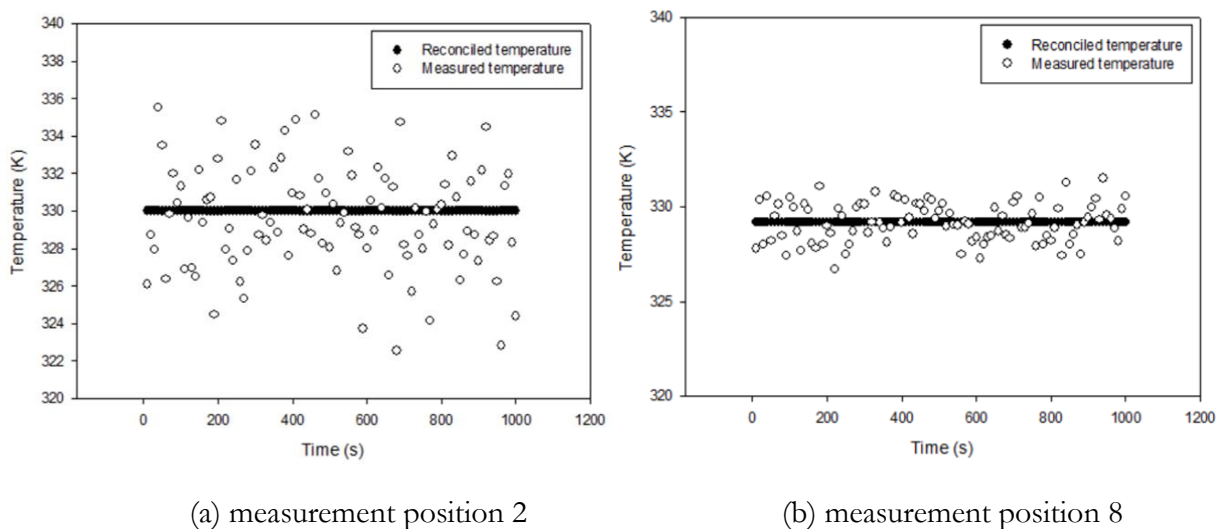


Fig. 5. Comparison between the simulation temperature and the temperature measured by the calibrated thermocouple.

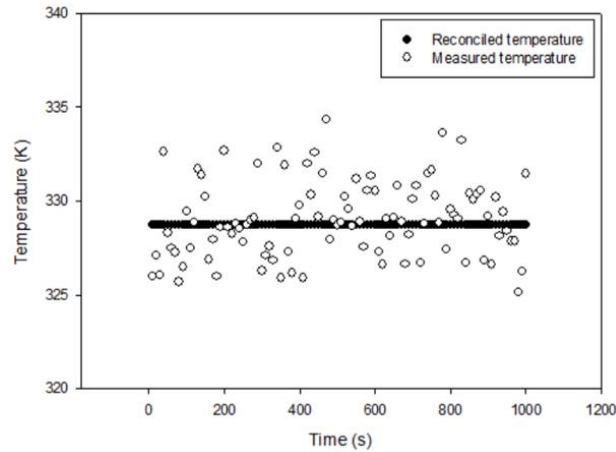
6.2. PDE-Based Data Reconciliation

In the real industry, the regular thermocouples usually contain the random errors in measurements. Therefore, the proposed data reconciliation approach has been developed to deal with the measurement errors. In this section, the regular thermocouples with random errors in measurements are used in order to test the effectiveness of the proposed data reconciliation approach. Figure 6 shows the values of the measured temperature and the reconciled temperature at the inlet (measurement position 2), within the domain (measurement position 8) and at the outlet (measurement position 17). It can be observed that the values of the measured temperature scatter around those of the reconciled temperature due to the effects of random errors.



(a) measurement position 2

(b) measurement position 8



(c) measurement position 17

Fig. 6. Measured and reconciled temperature at (a) measurement position 2 (b) measurement position 8 and (c) measurement position 17.

Figure 7 shows the averaged values of the measured temperature and the values of the reconciled temperature at different positions on the centerline. The error bars indicate ± 1.96 standard deviations of the mean. In contrast to the averaged values of the measured temperature, the PDE-based data reconciliation approach gives the reconciled temperature profile satisfying the PDE-based model.

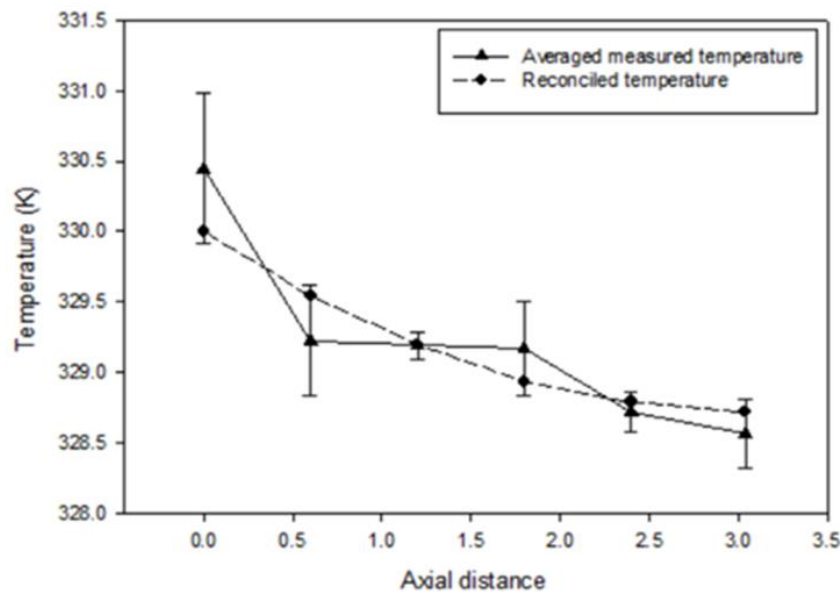


Fig. 7. Averaged measured temperature and reconciled temperature at different positions on the centerline.

Figure 8 shows the values of the reconciled temperature on the cross-sectional plane at axial position 1.5 m from the inlet. It can be observed that the values of the reconciled temperature decrease with increasing radial positions due to the transfer of heat in radial direction.

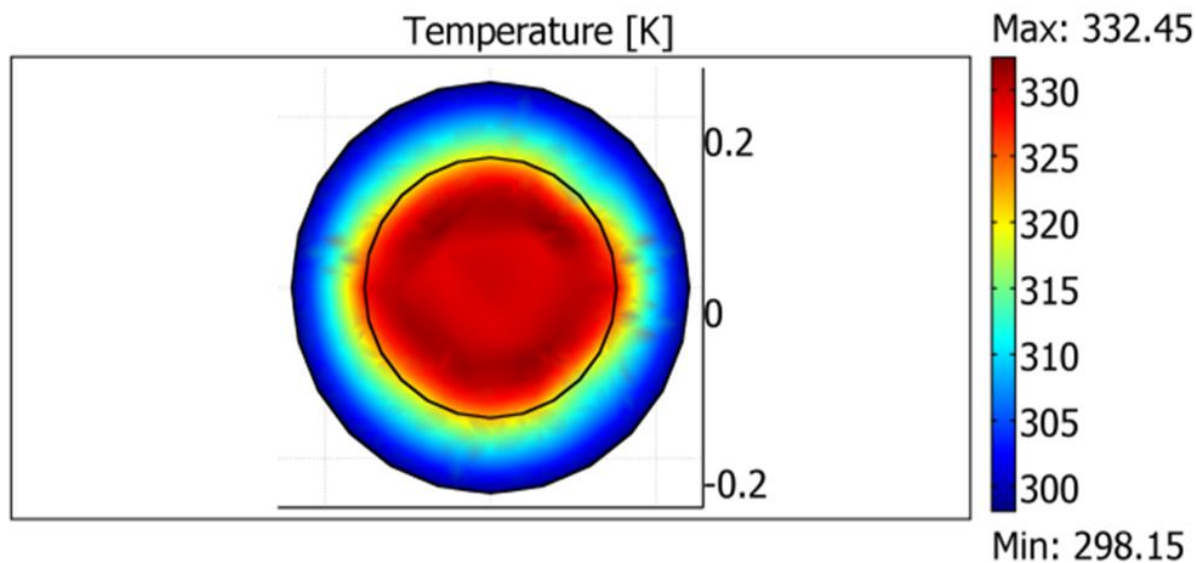


Fig. 8. Reconciled temperature on the cross-sectional plane at axial position 1.5 m from the inlet.

Figure 9 shows the values of the reconciled temperature on various cross-sectional planes. The temperature profiles on 5 cross-sectional planes are displayed. The proposed data reconciliation approach is based on the PDEs so the values of the reconciled temperature can be computed in axial and radial directions within the computational domain.

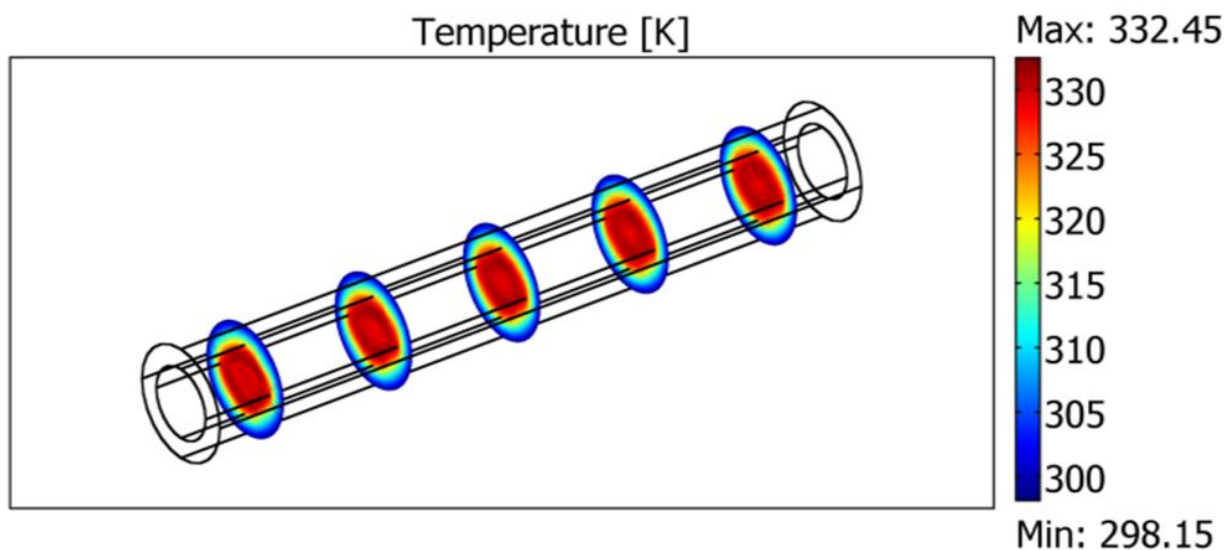


Fig. 9. Reconciled temperature on various cross-sectional planes.

The comparison between the PDE-based data reconciliation approach and the conventional data reconciliation approach [21] using the same type of the objective function (least-squares minimization) is shown in Table 4. Nearly the same values of the reconciled temperature at the inlet and outlet are obtained. In the conventional data reconciliation approach, however, the system is assumed to be lumped so the values of the reconciled temperature can only be computed at the inlet and outlet positions. Unlike the conventional data reconciliation approach, the PDE-based data reconciliation approach includes the variations of parameters within the system in order to describe the real system's behaviour. The values of the reconciled temperature can be computed within the computational domain as shown in Fig. 9.

Table 4. Comparison between the PDE-based data reconciliation approach and the conventional data reconciliation approach.

Approaches	Reconciled temperature at the inlet (PT2)	Reconciled temperature at the outlet (PT17)
PDE-based data reconciliation approach	330.00 K	328.78 K
Conventional data reconciliation approach [21]	331.05 K	328.45 K

The block diagram for the industrial applications of the proposed PDE-based data reconciliation approach is shown in Fig. 10. The proposed data reconciliation approach includes in the problem formulation the variations of parameters within the system in order to describe the real system's behaviour. The reconciled values can be computed within the computational domain so they can be used as the data in the troubleshooting, equipment analysis and maintenance of the industrial processes. Furthermore, the reconciled values can be used as the data in the process optimization.

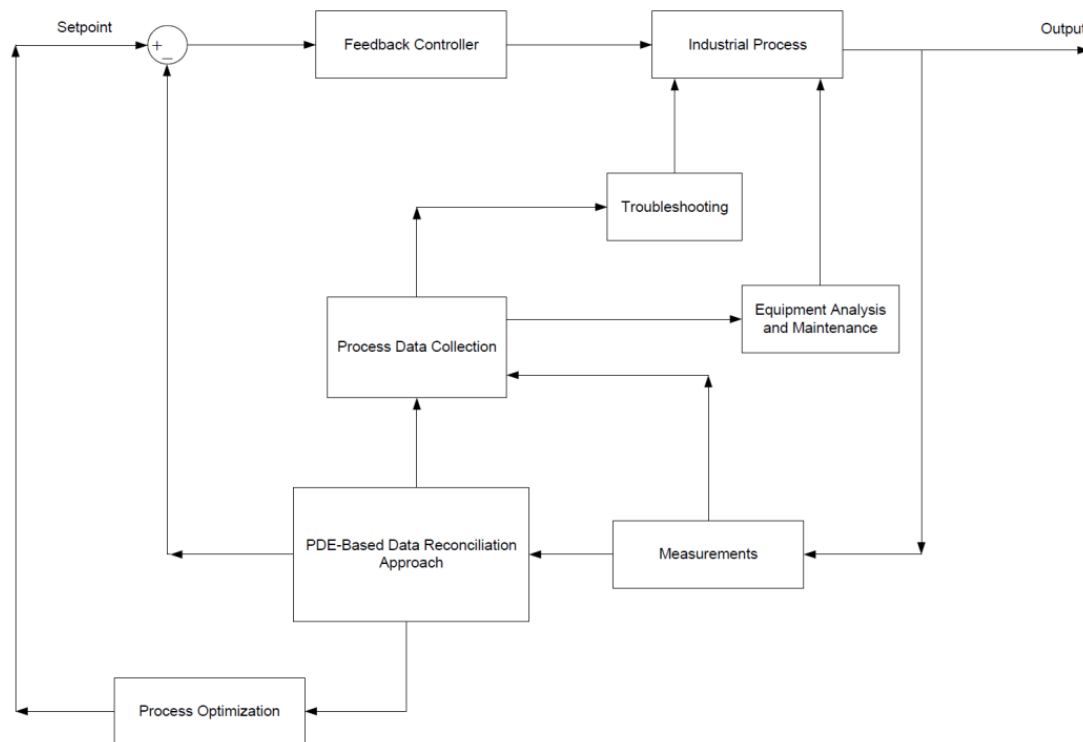


Fig. 10. Block diagram for the industrial applications of the proposed PDE-based data reconciliation approach.

Figure 11 shows the comparison between the values of the reconciled temperature at different positions on the centerline and the values of the temperature measured by the calibrated thermocouple. Although the measurement data with random errors are used as the input to the developed data reconciliation approach, the developed data reconciliation approach can calculate the values of the reconciled temperature that are in good agreement with the values of the temperature measured by the calibrated thermocouple. For this reason, the developed data reconciliation approach is useful in the real industrial applications.

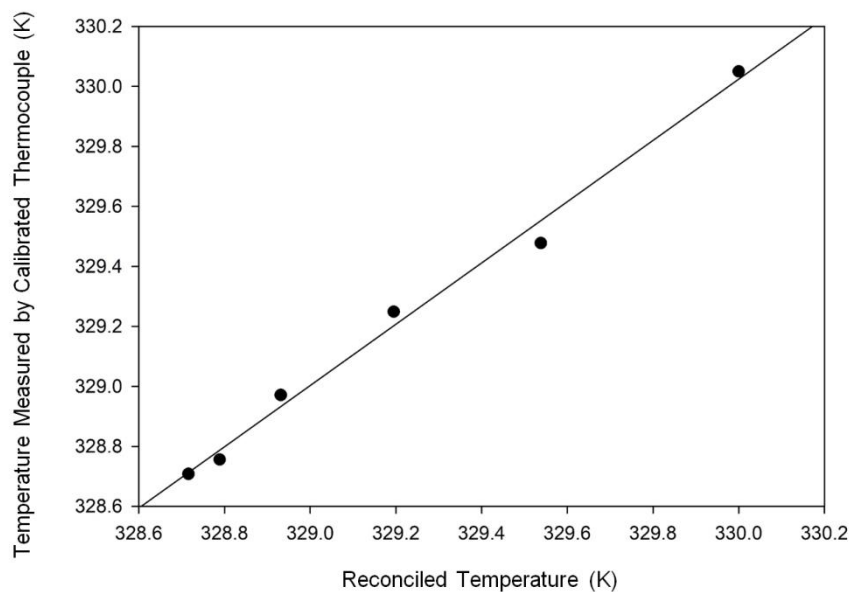


Fig. 11. Comparison between the reconciled temperature and the temperature measured by the calibrated thermocouple.

7. Conclusions

In this paper, the PDE-based data reconciliation approach has been developed to improve the quality of the measured data. Unlike the conventional data reconciliation approach in which the system is assumed to be lumped, the PDE-based data reconciliation approach includes in the problem formulation the variations of parameters within the system. The experiment is conducted to demonstrate the implementation of the developed data reconciliation approach. The values of the reconciled temperature can be computed within the computational domain based on the PDE-based model.

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