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Modelling of seed drying in fluidised and spouted bed dryers

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Abstract

Drying experiments were conducted in the fluidised bed dryer (FBD) and spouted bed dryer (SBD) at temperature 40-80°C using maize, rice and wheat seed samples. The experimental data were fitted into four thin-layer drying models by least square method. As a result, Page's model and two-compartment model were the best-fitted models. Due to the limitation of these models. Page's model and the twocompartment model were modified by adding the drying temperature term. Subsequently, these models could efficiently predict the drying curves under a wider range of temperatures with root mean square (RMS) of the MR_{predicted} - MR_{measured} not over 0.035.

Keywords: Drying model, Seed drying, Fluidised bed dryer, Spouted bed dryer, Drying air temperature

1. Introduction

To date, a number of drying models have been developed to estimate drying times. Several studies proposed simplified models for predicting the drying time of various products. Quite often, a semiempirical relationship, so-called "thin layer" equation that is analogous to Newton's law of cooling, was introduced to obtain the drying rate of food grains (Soponronnarit, 1997).

Initially, a thin-layer drying model was proposed by Lewis (1921). Regularly, Lewis's equation is referred to as the exponential model and is used for modelling the drying rate of biological materials. especially food grains (Ghaly and Sutherland, 1984; Byler et al., 1987; Shei and Chen, 1998). After Lewis's work, several thin-layer drying models have been developed for food materials (See summary in Table 1). Some researchers (Byler et al., 1987; Shivhare et al., 2000; Tan et al., 2001) claimed that Page's model could predict the drying behaviour of biological materials more accurately than the exponential model, and the relationship between the drying rate constant and air temperature could be represented by the Arrhenius law.

Another thin-layer drying model that has been widely used for modelling the drying of food grain is the 'two-compartment model'. It was found appropriate for application to paddy drying (Sharma et al., 1982; Noomhorm and Verma, 1986). Due to the uniformity of moisture and temperature of samples in FBD and SBD resembling the samples in thin-layer dryer, in this work, a number of thin-layer drying models were developed for maize, rice and wheat seeds dried in FBD and SBD. The aim of this research was to develop thin-layer drying models for predicting the drying curves of maize, rice and wheat seeds in FBD and SBD. These models were expected to be useful for the drying industry.

2. Materials and methods

2.1. Conditioning of seed samples

Australian paddy variety "Amaroo", wheat variety "Westonia", and waxy maize variety "33A63" were used in the experiments. These raw seed samples had moisture contents lower than the designed levels for drying experiments, therefore, seeds were rewetted by adding a calculated amount of distilled water. Seeds were then mixed daily and kept at a temperature of 2-5°C for about 7 d to allow for mosuture equilibration within the seed and to avoid spoilage. The moisture content of seed samples was determined in accordance to ASAE standards (ASAE, 1988).

2.2. Drying experiments

Drying experiments were conducted in two types of dryers consisting of FBD and SBD as outlined in Table 1. During drying experiments, seed samples were collected in each time step for moisture content determination. The data of moisture content change of rice, maize and wheat seeds under each drying condition were used for the purpose of model development.

 Table 1
 Summary of conditions used in drying experiments

Drying method	Materials	Studied conditions	Remarks
Fluidised bed drying	Maize, rice and wheat seeds	Three levels of initial moisture content (20, 23, 25%wb) and three levels of temperature (40, 60, 80 °C).	Bed depth 0.1 m. Air velocity ≈ 2.8-3.0 m/s. The FBD was designed and constructed at the UNSW, Dept. Food Science & Technology.
Spouted bed drying	Rice and wheat seeds	Three levels of initial moisture content (20, 23, 25%wb) and three levels of temperature (40, 60, 80 °C).	Use sample amount equal to that used in FBD experiment. Air velocity ≈ 8-10 m/s. SBD and its accessories were designed and constructed at the UNSW, Dept. Food Science & Technology.

2.3. Drying model development

Data from drying experiments were fitted into four thin-layer drying models, consisting of Page's model, two-compartment model, Wang and Singh's (1978) model and exponential model (see Table 2) by least square method. The software Statistica 5.5 StatSoftTM (StatSoft Inc., Tulsa, OK, USA) was used for model fitting. In developing thin-layer drying models, the required data consisted of initial moisture content, seed moisture content during drying process, seed equilibrium moisture content, temperature and relative humidity of drying air, and drying time. Equilibrium moisture contents were calculated by using the equations in Table 3 while the other data were obtained from the experiments.

Table 2 List of thin-layer drying models used in this study

Models	References
Lewis's model (Exponential model)	Lewis, 1921; Ghaly and Sutherland,
$MR = (M-M_e)/(M_i-M_e) = exp(-kt) k = drying constant$	1984; Shei and Chen, 1998
Two-compartment model	Henderson, 1974; Sharaf-Elden et
$MR = (M-M_e)/(M_i-M_e) = Ae^{-k_1t} + Be^{-k_2t} A, B, k_1, k_2 = drying constants$	al., 1980
Thompson's model	Thompson et al., 1968
$t = A(\ln(MR)) + B(\ln(MR))^2 A$, B = drying constants	Thompson et al., 1906
Page's model	ASAE, 1995; Sogi et al., 2003
$MR = (M-M_e)/(M_i-M_e) = \exp(-kt^N) k = f(air temp, air velocity) N = f(initial MC, RH)$	ASAE, 1995, Sogi et al., 2005
Wang and Singh's model	Wang and Singh 1079
$MR = (M-M_e)/(M_i-M_e) = Aexp(-kt) A,k = drying constants$	Wang and Singh, 1978

 Table 3
 Equations used for estimating the equilibrium moisture content of seeds

Product	Equations	References	Remarks
	1 / ln(1 - RH) \13856		Where
Maize	$M_{\circ} = \frac{1}{100} \left(\frac{100}{-0.00003074(T + 273.15)} \right)$	Pudpong et al., 1990	M_e = Equilibrium moisture
Rice	M_e =	Steffe and Singh, 1980	content (db, decimal)
Rice	w _e	Stelle and Siligil, 1980	RH = Relative humidity of
Wheat	M.=	Bakker-Arkema et al., 1978	air, decimal
	e		T =Inlet air temperature, °C

3. Results

There were two major groups of drying models developed in this work namely models for FBD and those for SBD.

3.1. Drying models for FBD

Thin-layer drying models were developed for seeds of each of the three crops and each drying temperature. The coefficients of determination (R²) and mean residual square (MRS) were calculated for each drying treatment and crop. The highest values of R² and the lowest of MRS were obtained for the Page's and two-compartment models. The results are shown in Tables 4 and 5. These models were not particularly useful because each could be used for one specified drying temperature.

 Table 4
 Page's model for FBD

Product	Drying air temperature (°C)	Page's model	\mathbb{R}^2	MRS
	40		96.20	5.2E-04
Maize	60		98.10	4.7E-04
	80		97.72	1.1E-03
	40		98.33	7.4E-04
Rice	60		99.40	3.9E-04
	80		98.60	9.2E-04
	40		98.85	5.7E-04
Wheat	60		98.37	1.1E-03
	80		98.31	1.2E-03

Table 5 Two-compartment model for FBD

Product	Drying air temperature (°C)	Two compartment model	\mathbb{R}^2	MRS
	40		95.14	6.6E-04
Maize	60		97.75	5.6E-04
	80		96.91	1.4E-03
	40		98.44	7.0E-04
Rice	60		98.96	6.8E-04
	80		99.09	6.0E-04
	40		98.68	6.5E-04
Wheat	60		98.66	8.6E-04
	80	<u></u>	99.29	5.2E-04

Thus, two additional models were developed by modifying Page's and two-compartment models; a term for drying air temperature was added (Table 6). In fitting each modified model, the entire range of experimental data between 40 and 80°C drying air temperatures were used (Tables 7 and 8).

 Table 6
 Modifications to Page's and modified two-compartment model

Description	Equations	Remarks
Modified Pages model	$MR = (M-M_e)/(M_i-M_e)$ = exp(-kt ^N exp(-B/T _K))	Where MR = Moisture ratio
	$= \exp(-\kappa t \exp(-B/T_K))$	M = Moisture content of sample at time t (db), decimal
Modified two- compartment model	$MR = (M-M_e)/(M_i-M_e)$ = $A_1 \exp(-k_1 t \exp(-B/T_K))$ + $A_2 \exp(-k_3 t \exp(-B/T_K))$	M_e = Equilibrium moisture content (db), decimal M_i = Initial moisture content of sample (db), decimal T_K = Drying air temperature (K)
	/ 1/2 exp(-k2t exp(-b/ 1k))	t = Drying time (minutes) k, k ₁ , k ₂ , A ₁ , A ₂ , B, N = Drying constants

 Table 7
 Modified Page's model for FBD

Product	Drying air temperature (°C)	Modified Page's model	\mathbb{R}^2	MRS
Maize	40-80		98.07	6.9E-04
Rice	40-80		98.57	9.4E-04
Wheat	40-80		98.26	1.2E-03

 Table 8
 Modified two-compartment model for FBD

Product	Drying air temperature (°C)	Modified two-compartment model	\mathbb{R}^2	MRS
Maize	40-80		97.11	1.0E-03
Rice	40-80		98.38	1.1E-03
Wheat	40-80		98.75	8.8E-04

The comparison between the experimental data and the models for FBD (Page's, two-compartment, and modified Page's and modified two-compartment) is shown in Figure 1. There is a good agreement between the experimental and the model-predicted values for all models. Additionally, there is a slight improvement in the agreement between experimental and model predicted values for the modified models.

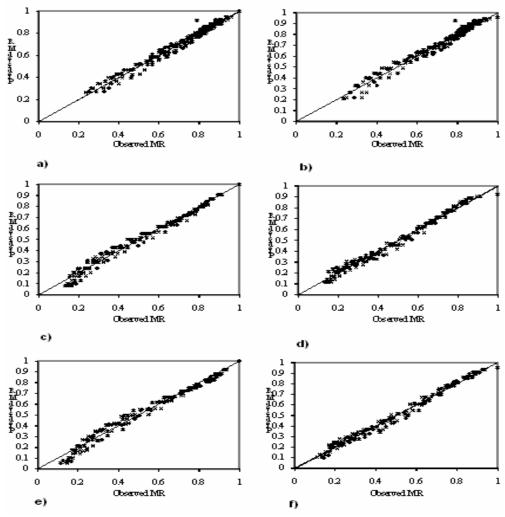


Figure 1 Comparison between MR_{observed} and MR_{predicted} in FBD: a) Maize, modified Pages model b) Maize, modified two compartment model, c) Rice, modified Pages model d) Rice, modified two compartment model e) Wheat, modified Pages model f) Wheat, modified two compartment model

3.2. Drying models for SBD

Best drying results of model fitting for both FBD and SBD were obtained using Page's and two-compartment model (Tables 9 and 10). As explained previously, these two models were modified to allow use over a wide range of drying air temperatures (between 40 and 80°C). The modified models are shown in Tables 11 and 12.

 Table 9
 Page's models for SBD

Product	Drying air temperature (°C)	Page's model	\mathbb{R}^2	MRS
	40	-	98.97	3.4E-04
Rice	60	-	99.27	4.8E-04
	80	-	98.80	9.5E-04
	40	-	98.88	4.4E-04
Wheat	60	-	98.63	9.3E-04
	80	-	98.81	1.1E-03

Table 10 Two compartment models for SBD

Product	Drying air temperature (°C)	Two compartment model	\mathbb{R}^2	MRS
	40	-	99.07	3.1E-04
Rice	60	-	99.42	3.8E-04
	80	-	99.68	2.5E-04
	40	-	98.92	4.3E-04
Wheat	60	-	98.84	7.9E-04
	80	-	99.62	3.5E-04

Table 11 Modified Page's model for SBD

Product	Drying air temperature (°C)	Modified Page's model	\mathbb{R}^2	MRS
Rice	40-80	-	98.78	8.5E-04
Wheat	40-80	-	98.81	8.5E-04

Table 12 Modified two-compartment model for SBD

Product	Drying air temperature (°C)	Modified two-compartment model	\mathbb{R}^2	MRS
Rice	40-80	-	99.44	3.9E-04
Wheat	40-80	-	99.17	5.9E-04

The comparison between the experimental data and the models for SBD (Page's, two-compartment, and modified Page's and modified two-compartment) is shown in Figure 2. There is good agreement between the experimental and model-predicted values for all models with an overall better agreement for the modified models.

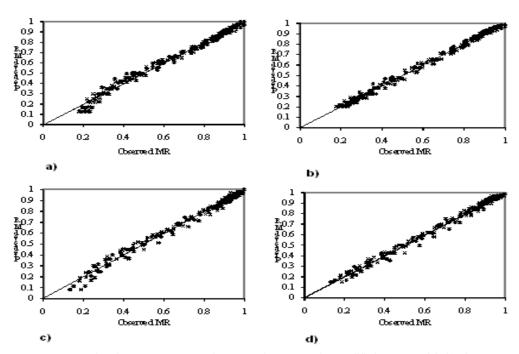


Figure 2 Comparison between MR_{observed} and MR_{predicted} in SBD: a) Rice, modified Page's model; b) Rice, modified two compartment model; c) Wheat, modified Page's model; d) Wheat, modified two compartment model

4. Discussion

Based on the results of this study, the modified drying models for both types of dryers could accurately predict drying curves for maize, rice and wheat seed under a range of drying temperature from 40-80°C with the MRS values of deviations between predicted moisture ratio and the measured values (MR $_{predicted}$ - MR $_{measured}$) being ≤ 0.0012 (or RMS ≤ 0.035). Moreover, because these models were not complicated, users can use them on scientific calculators or personal computers.

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