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Thermolysis of plastic waste: Reactor comparison

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Thermolysis of plastic waste:

Reactor comparison

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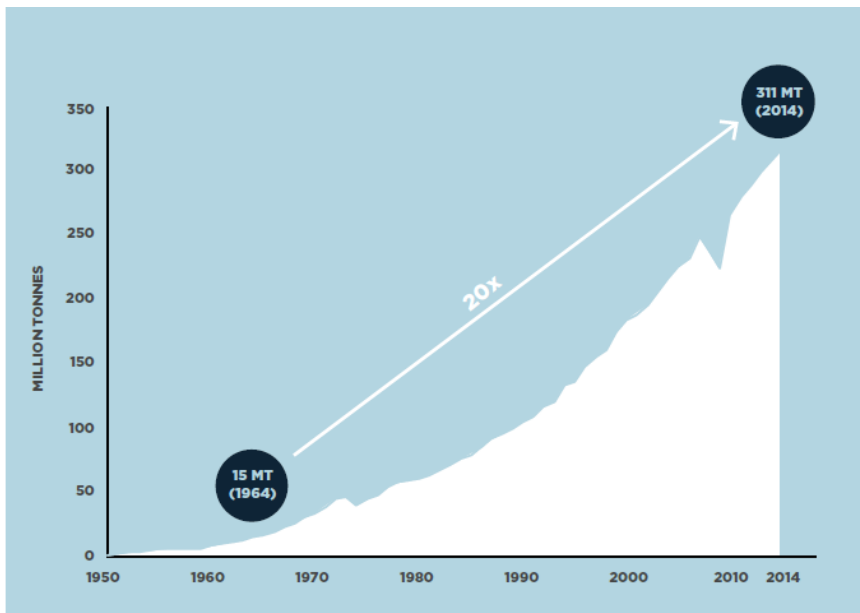
Pyroliq 2019, Cork, Ireland

Contents

- Thermolysis of plastic waste
- Common types of reactors
- Commercial systems
- Factor affecting product spectrum
- Lessons learnt



Plastic demand



Note: Production from virgin fossil-based feedstock only (does not include bio-based, greenhouse gas-based or recycled feedstock).

Source: PlasticsEurope, *Plastics - the Facts 2013* (2013); PlasticsEurope, *Plastics - the Facts 2015* (2015).



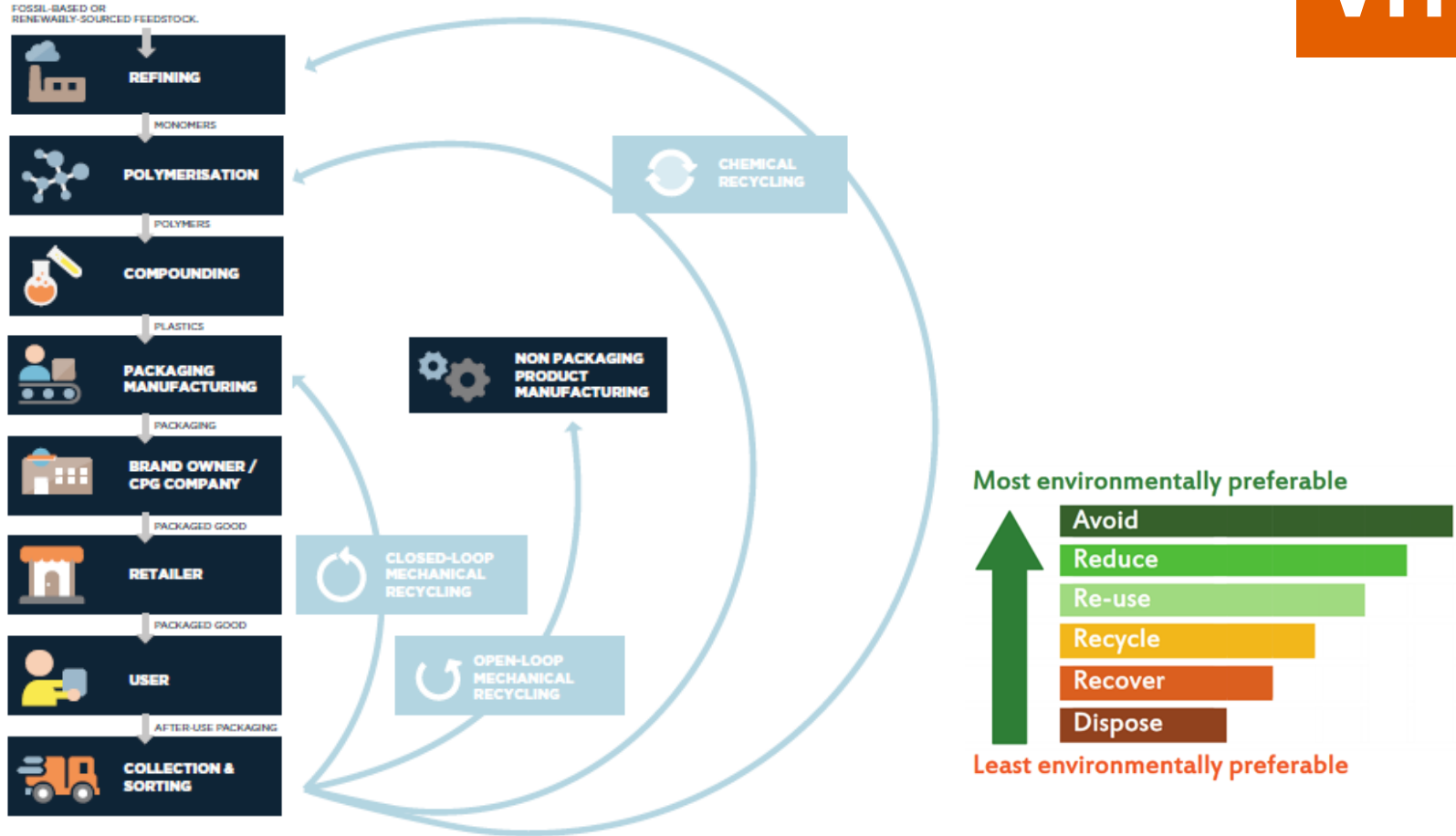
Plastic demand by sector - Europe



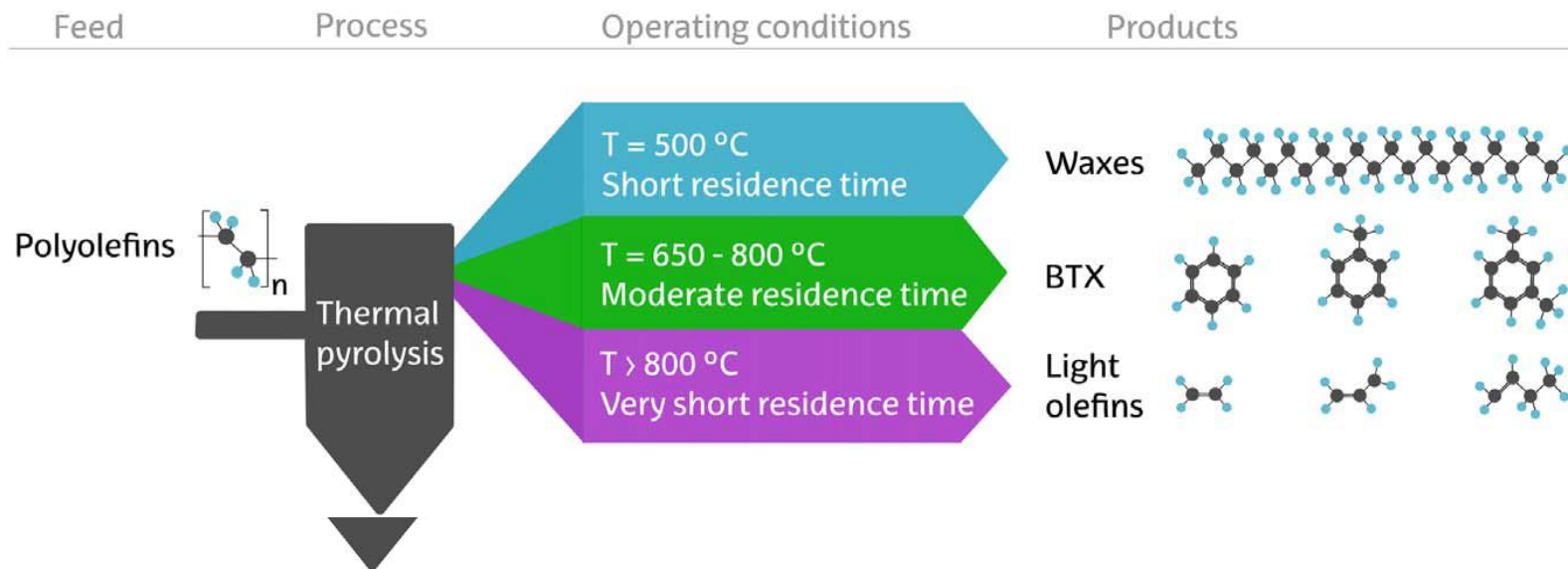
Plastic waste come in all shapes and sizes and usually not alone...



Plastic recycling options

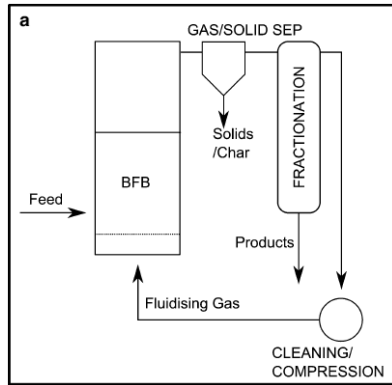


Typical thermolysis products

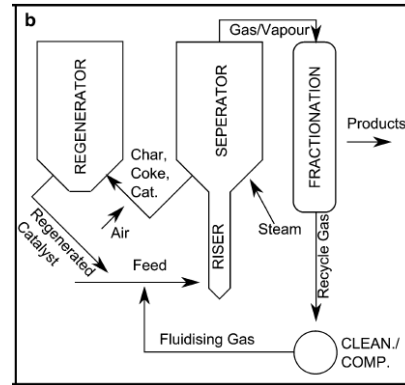


Conditions for the selective production of waxes, BTX (Benzene, Toluene and Xylene) and light olefins from polyolefins by thermal cracking.

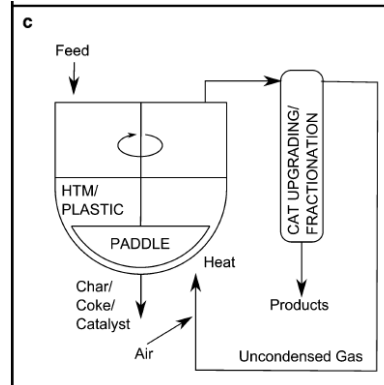
Common reactors for plastic thermolysis



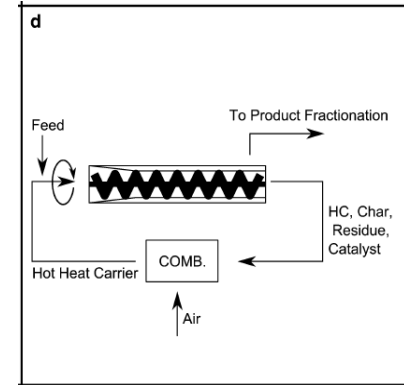
Fluidized bed



Fluid catalytic cracking



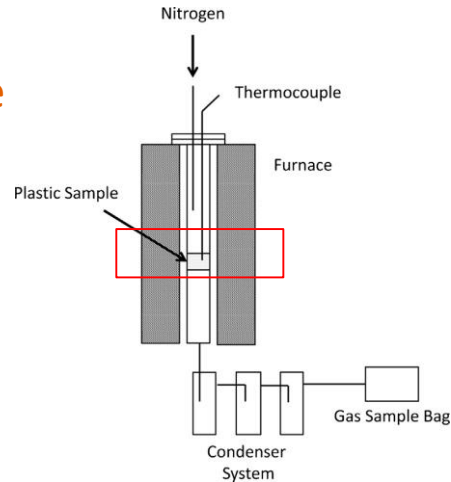
CSTR reactor



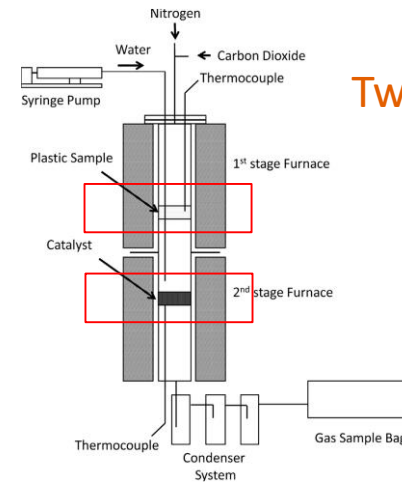
Screw reactor

1. Fixed bed reactors

Single stage

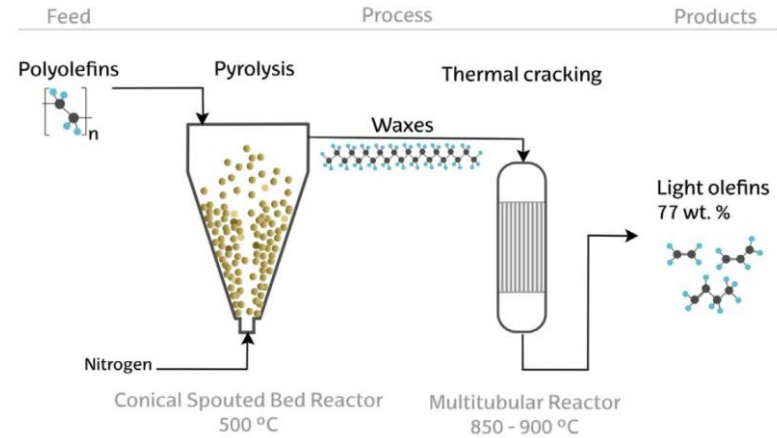
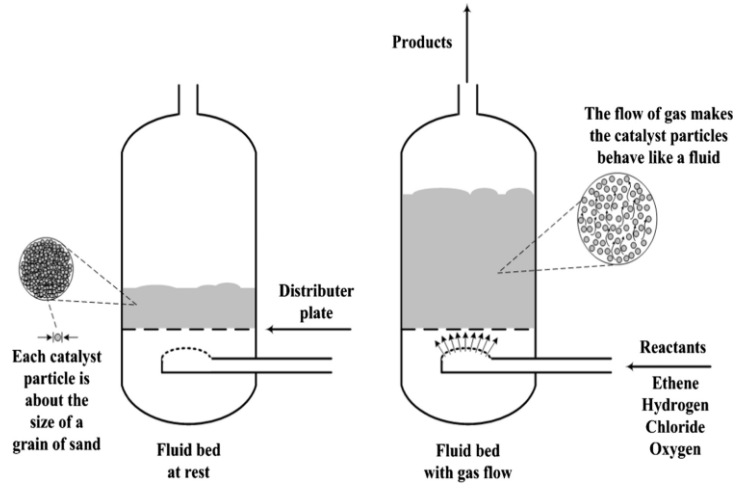


Two stage



Advantages	Disadvantages
Simple construction and easy to build	Temperature controls are difficult
Economical operation and maintenance of the unit	Batch operation and scale up issues
Two staged process for selective productions	Bed channelling causes uneven distribution of products
Both thermal and catalytic processes are possible	Coke deposition causes blockages and increase pressure drop

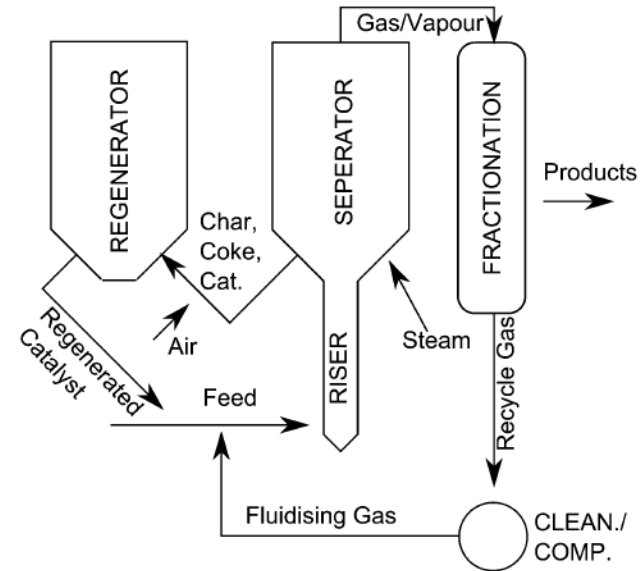
2. Fluidized bed reactors



Advantages	Disadvantages
High heat and mass transfer and solid mixing regimes	Complex design and operation
Significant versatility on gas residence times	Bed defluidization may occur
Liberty in product distribution – residence time	Melt plastic attaches to the surface of the bed particles.
Continuous operation possible (scalable)	A pilot plant is often necessary for scale up
Both thermal and catalytic processes are possible	Attrition of particle can be serious in CFB
Maintenance costs are moderate	Capital costs are higher for CFB than BFB

3. Fluid Catalytic Cracking (FCC)

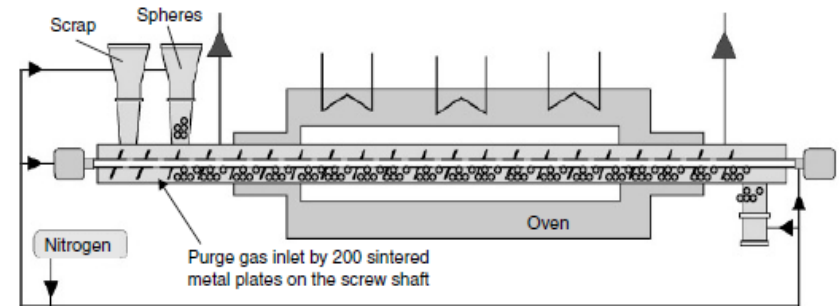
- Widely used in conventional refinery (VGO to gasoline)
- Two zones in the reactor
 - Hot particulate catalyst contact with feed creating cracking products and coked catalyst
 - Catalyst is regenerated by burning
 - Hot catalyst is recycled to the riser for additional cracking of feed
- Feedstocks are cracked to gaseous components and further separated to fuel gas,
- Large energy requirement
- Good solid polymer mixing



Schematic FCC unit

4. Screw/Auger kiln reactors

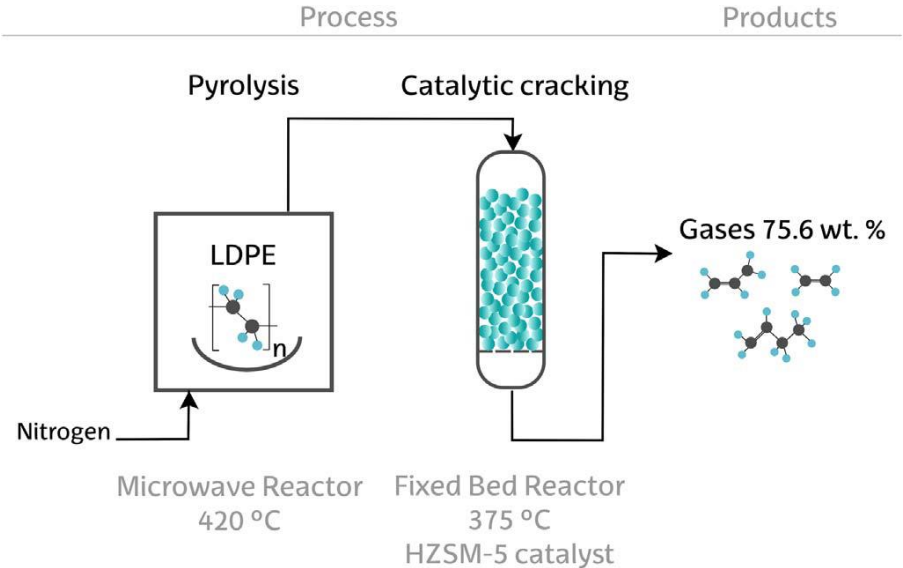
- Typically made up of tubular reactor and a screw conveyor.
- Residence time can be varied by the varying the speed of the screw and length of the reactor
- Spheres (metal/ceramic) avoid coke build up and improves heat transfer.
- High amounts of thermoset materials (e.g. WEEE) can be pyrolyzed
- Efficient removal of chlorine from the mixed waste
- Selective zone heating from outside.
- Several Rotary kiln commercial process are online (feedstocks biomass, municipal solid waste, Tires, shredder light fractions, WEEE, cables etc.)



Haloclean process

5. Microwave thermolysis

- Attractive for efficient heat transfer
- Plastic has to be mixed with heat adsorbent such as graphitic carbon or inorganic oxides
- Temperatures can reach up to 1000 °C
- Short residence time
- Poor mixing
- Scale up is questionable

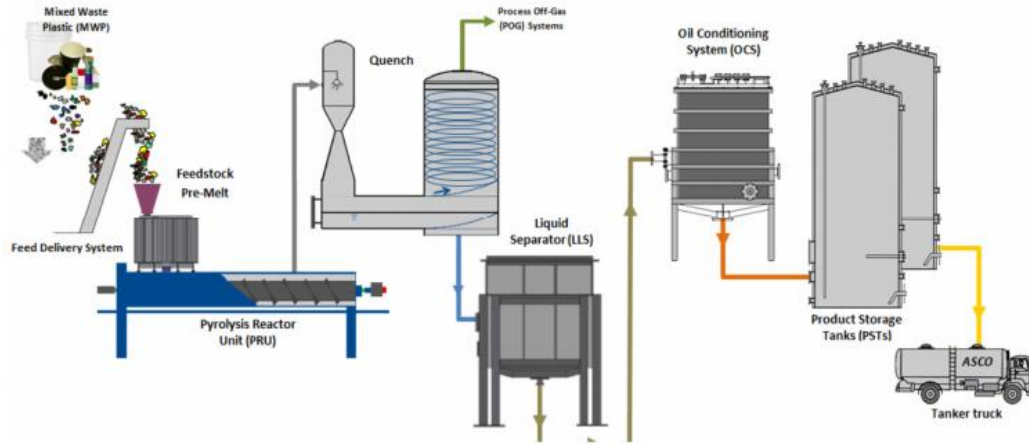


LOPEZ, G., ARTETXE, M., AMUTIO, M., BILBAO, J. and OLAZAR, M., 2017. Thermochemical routes for the valorization of waste polyolefinic plastics to produce fuels and chemicals. A review. *Renewable and Sustainable Energy Reviews*, 73, pp. 346-368

Commercial systems



Agilyx (USA) – Screw reactor

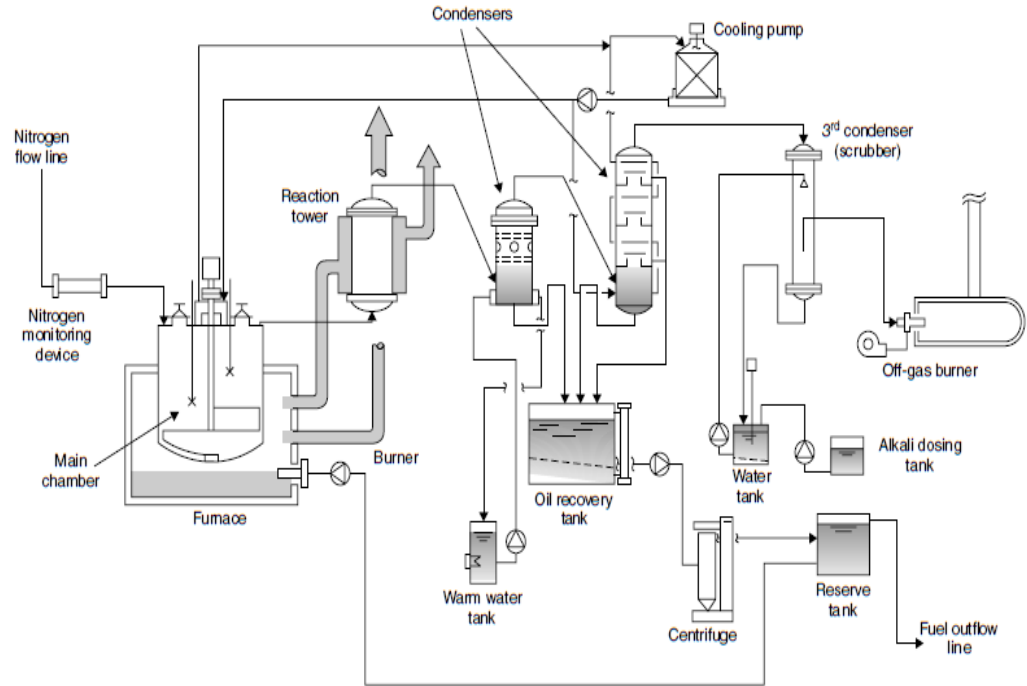


Schematic flow diagram of the Agilyx process

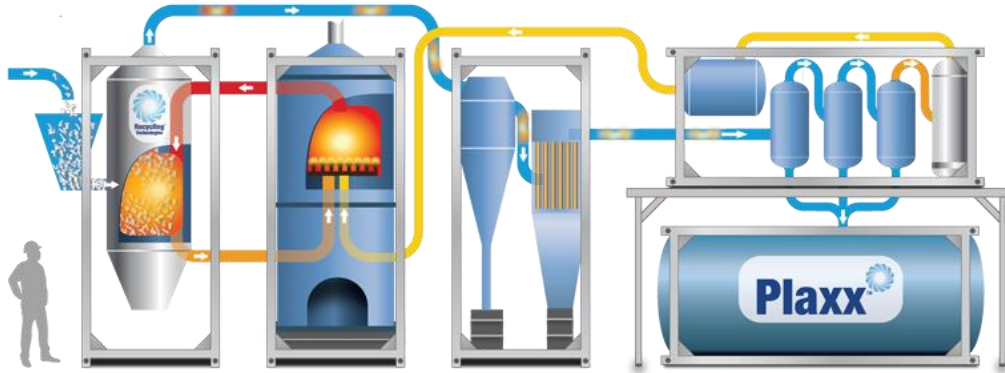
- Continuous non-catalytic
- Self cleaning dual screw reactor
- Currently operational 10 TPD, pilot scale
- Light sweet synthetic crude is the main product sold to a refinery

Plastic energy (Spain) - CSTR

- Thermal degradation in STR
- Moderate temp (320-425°C)
- Vapor phase upgrading at 220°C
- Several plants in Japan, Ireland, UK and Spain
- 20 TPD available



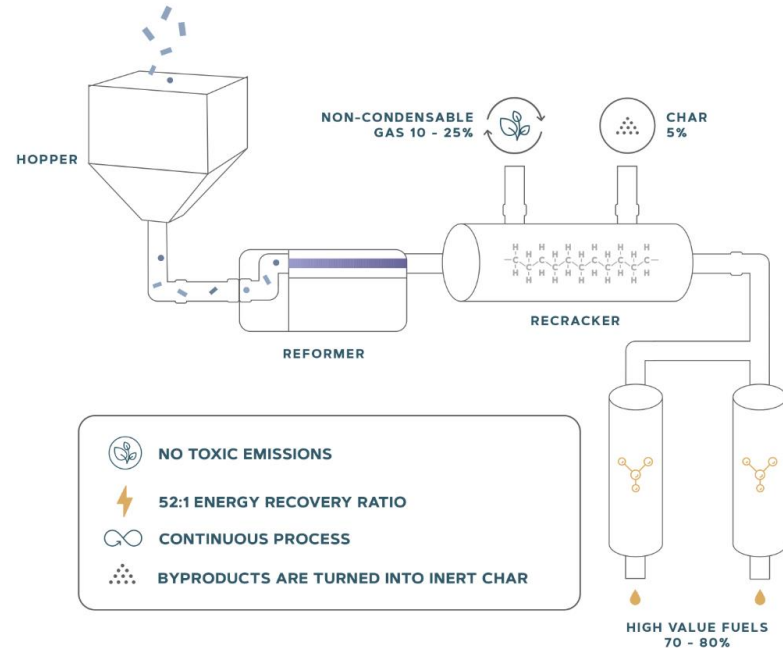
Recycling technologies (UK) – Circulating Fluidized bed



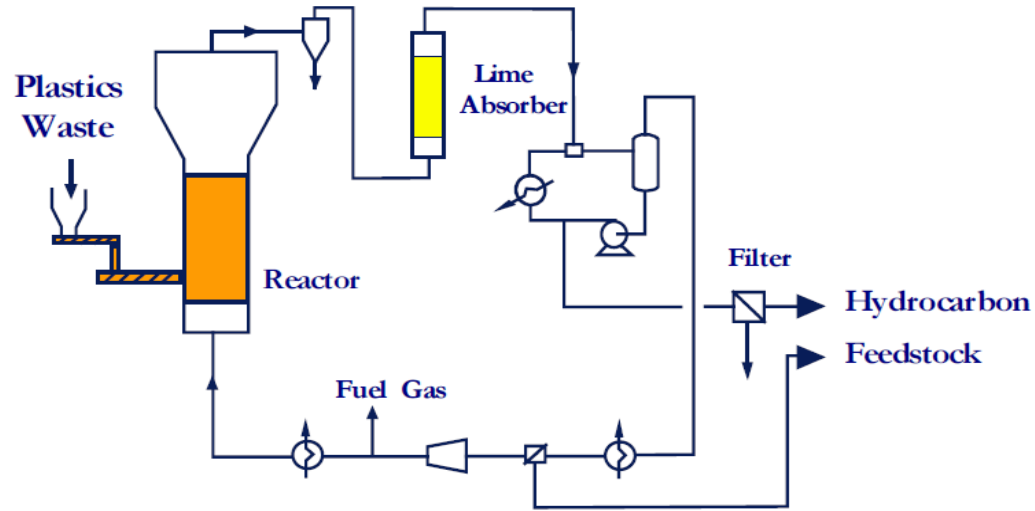
- Advanced fluidized bed reactor, the RT7000, uses thermal depolymerization
- residual plastic waste from material recycling facilities (MRFs) as feedstock
- Plaxx™ is a hydrocarbon product, low sulphur alternative to heavy fuel oil (HFO).
- Dry weight capacity 7000 tpa

Renewlogy (USA) – Auger / Kiln reactor

- Plastic is dried and shredded
- Auger/kiln reactor
- Easy control over product
- Output ranging from wax to crude-like oil to diesel-quality oil.
- Renewlogy– Nova Scotia Canada set up a large plastic conversion system at their site in 2017
- 10 TPD modules



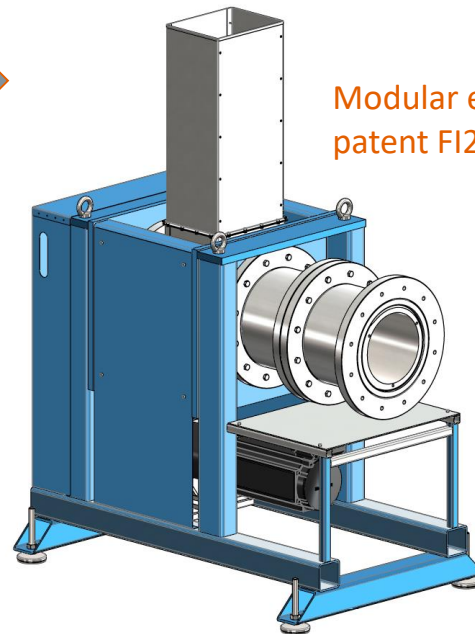
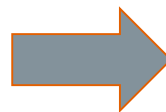
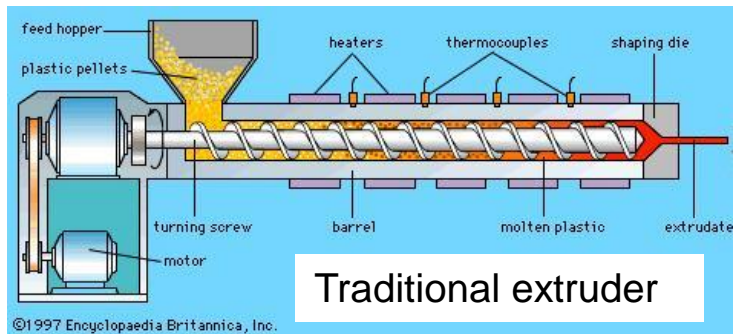
BP process (Hamburg) – Fluidized bed reactor



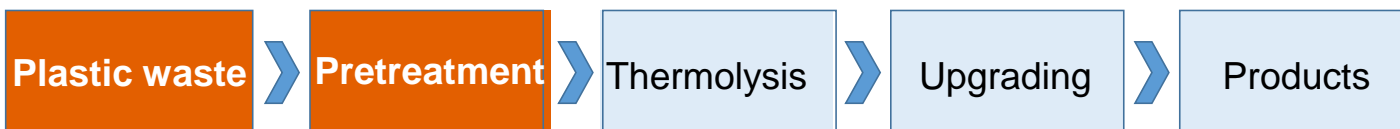
Schematic representation of the BP process.

- Low temperature (500° C) thermal fluidized bed process
- Dechlorination using lime absorber
- Light and heavy wax was the main product
- (50 kg/h) plant no longer operational

Integrated material pretreatment to thermolysis



- Heterogenous feed including foils which otherwise are difficult to process
- Processing to granules or straight to thermolysis as melt compound



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Reactor comparison for plastic thermolysis

	Temp. control	Heat transfer	Particle size flexibility	Residence time flexibility	Process flexibility	Thermal mode operation	Catalytic mode operation	Value of obtained products	Scale-up flexibility	Economic feasibility
Fixed Bed	Red	Red	Yellow	Yellow	Red	Yellow	Yellow	Green	Red	Yellow
BFB	Yellow	Green	Yellow	Yellow	Green	Green	Green	Green	Yellow	Yellow
CFB	Yellow	Green	Yellow	Yellow	Green	Green	Yellow	Green	Yellow	Red
Rotary kiln	Red	Red	Yellow	Green	Yellow	Green	Yellow	Yellow	Yellow	Yellow
Melting vessel	Red	Red	Yellow	Green	Yellow	Green	Yellow	Yellow	Yellow	Red
Extruder	Yellow	Red	Red	Red	Green	Yellow	Yellow	Green	Green	Yellow

Green = good

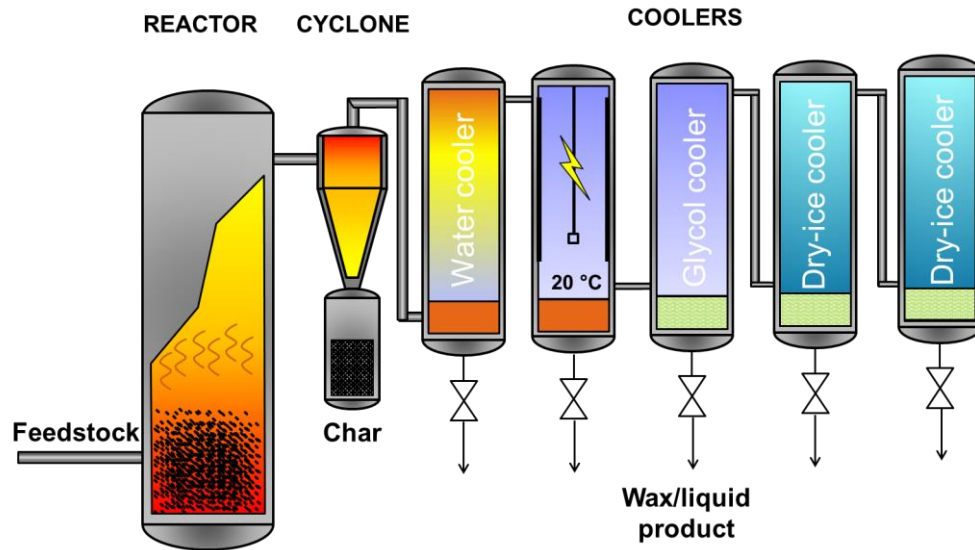
Orange = satisfactory

Red = Poor

Factors affecting product distribution

- **Temperature**
 - Lower temperatures ($T < 700^{\circ}\text{C}$) yield solids and waxes/oil whereas higher temperatures favour gas formation
- **Pressure**
 - The effect of pressure is dominant at lower temperatures and reduces with an increase in temperature
- **Heating rate**
 - Higher heating rate - bond cleavage, lower heating rate - char formation
- **Feedstock composition**
 - Varying products with varying feedstocks (PVC and PET unappreciable)
- **Residence time**
 - Longer residence times light molecular weight hydrocarbons and non-condensable gases
- **Reactor type**: Different reactors different product distribution

Thermolysis reactor (BFB) - VTT

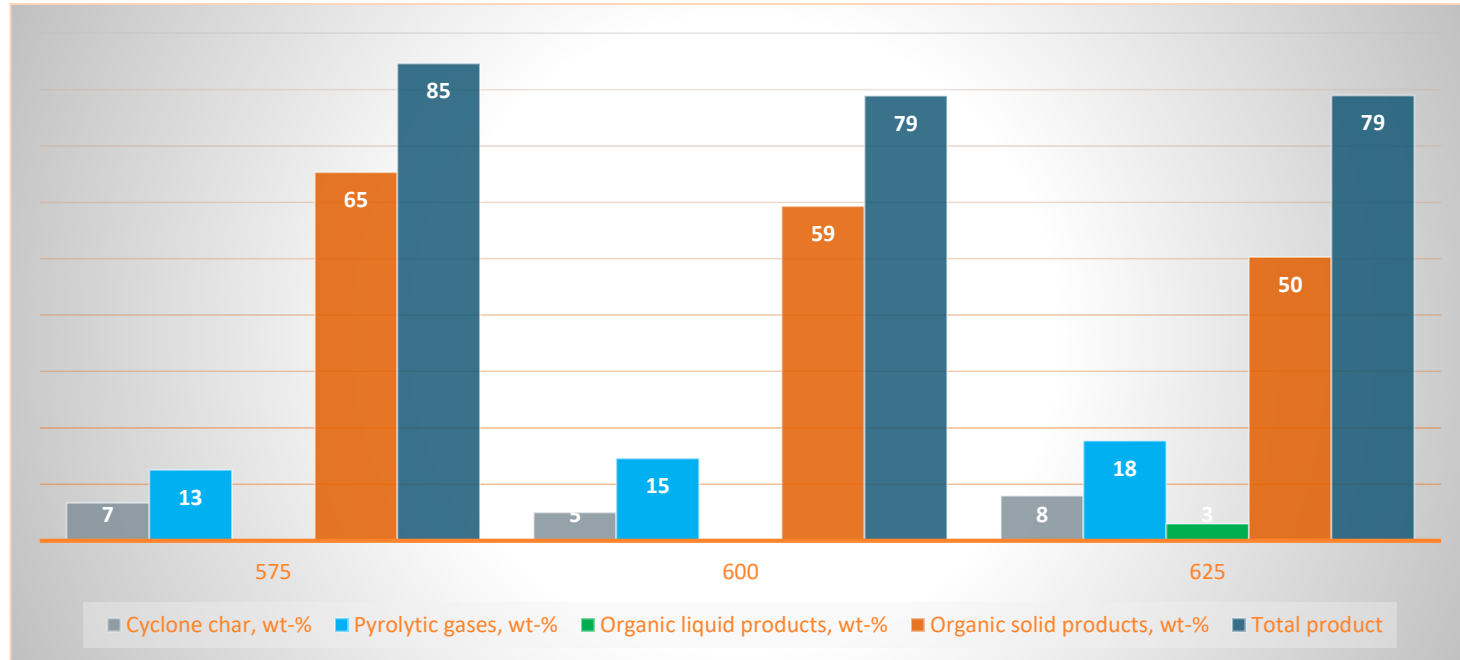


Features:

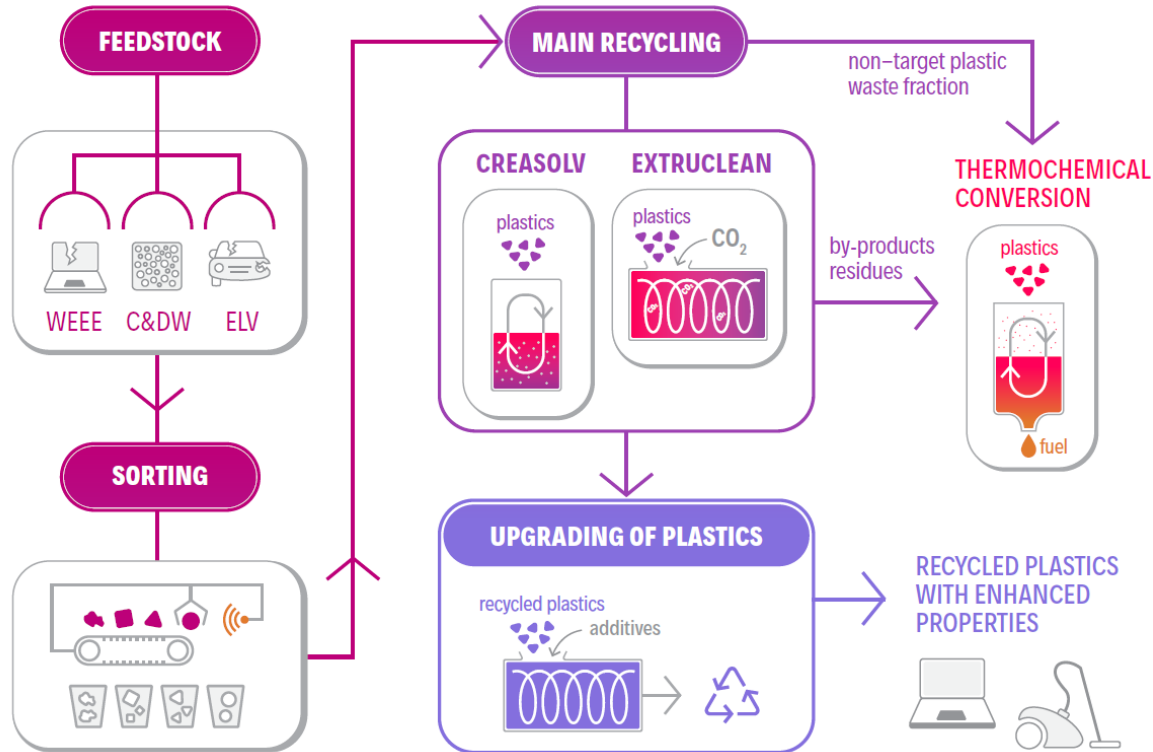
- Feed capacity : 1kg/hr
- Operating temperatures ~ 500 – 700 C
- Feeder : Screw feeder
- Condenser: 1 water cooler, 1 glycol cooler, 2 dry ice coolers

Online gas chromatographic analysis

Thermolysis trials- Reject from plastic recycling



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