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Upgrading of wheat/barley and miscanthus bio-oil over a sulphided catalyst

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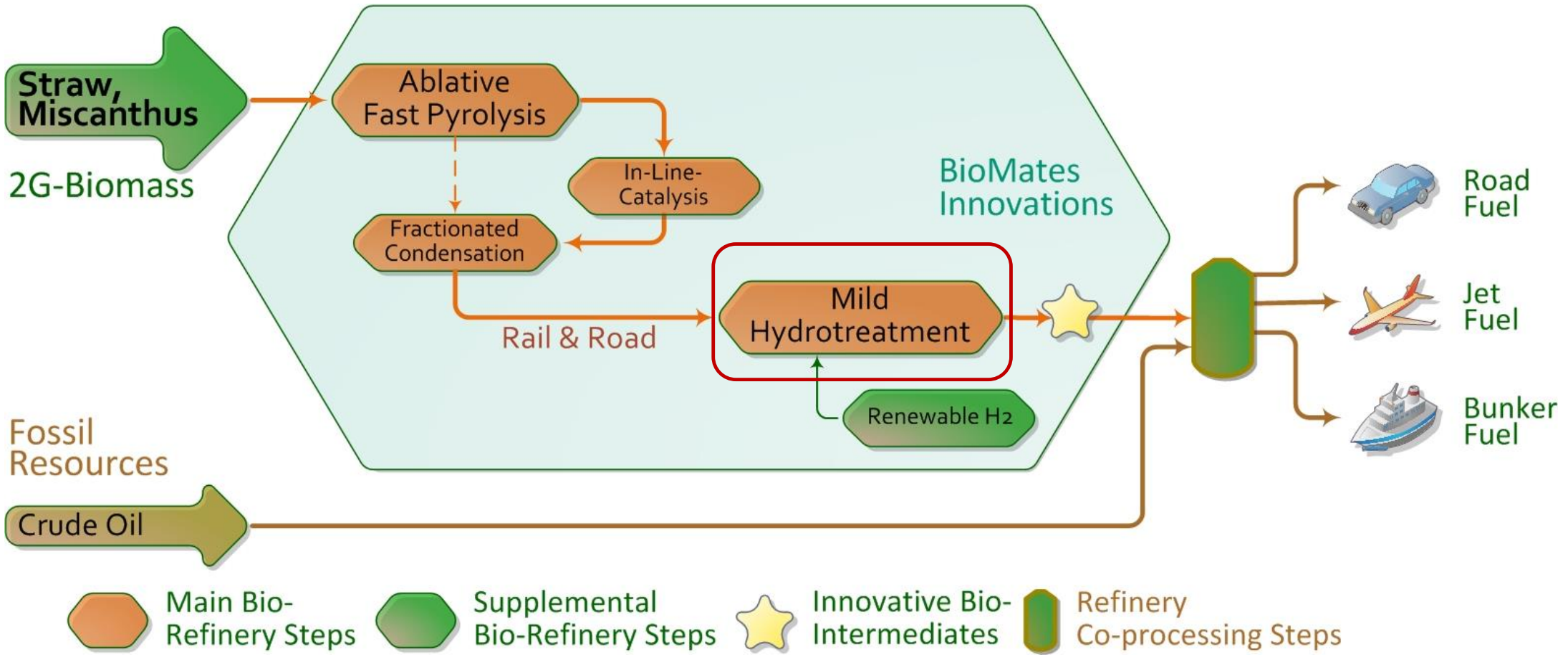
BioMates

Upgrading of wheat/barley straw bio-oil over a sulphided catalyst

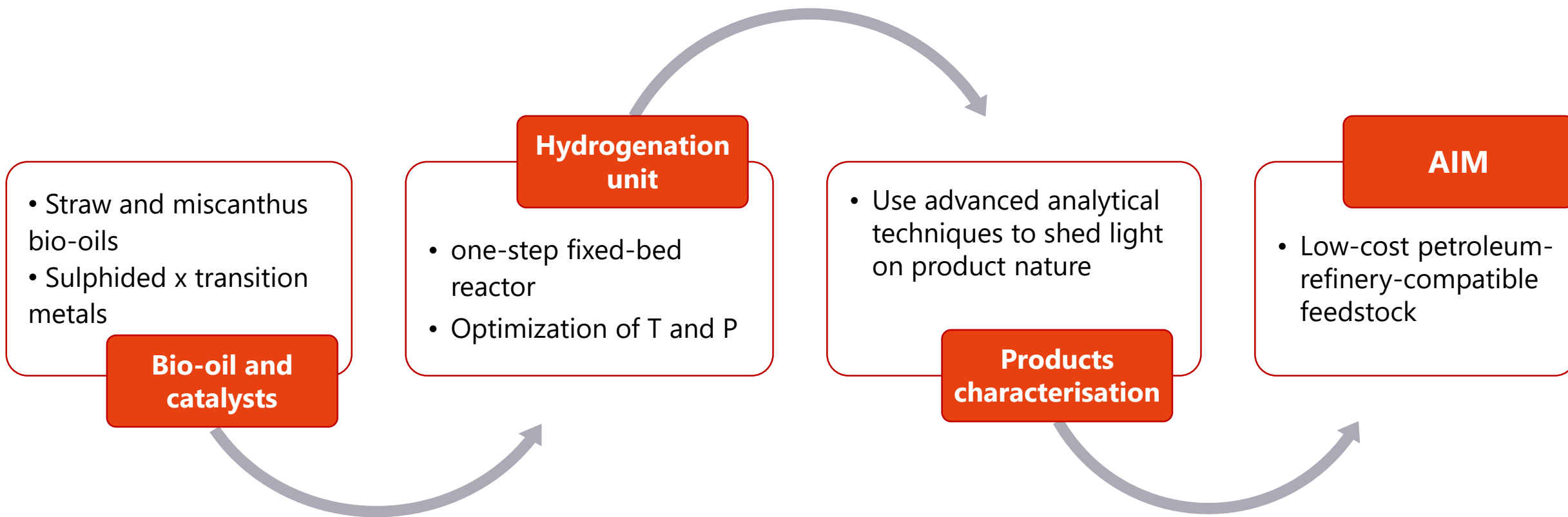
Shumeiko Bogdan, David Kubička, Miloš Auersvald, Petr Straka, Dan Vrliška, Pavel Šimáček

Cork, Ireland

19/06/2019



Source: www.biomates.eu





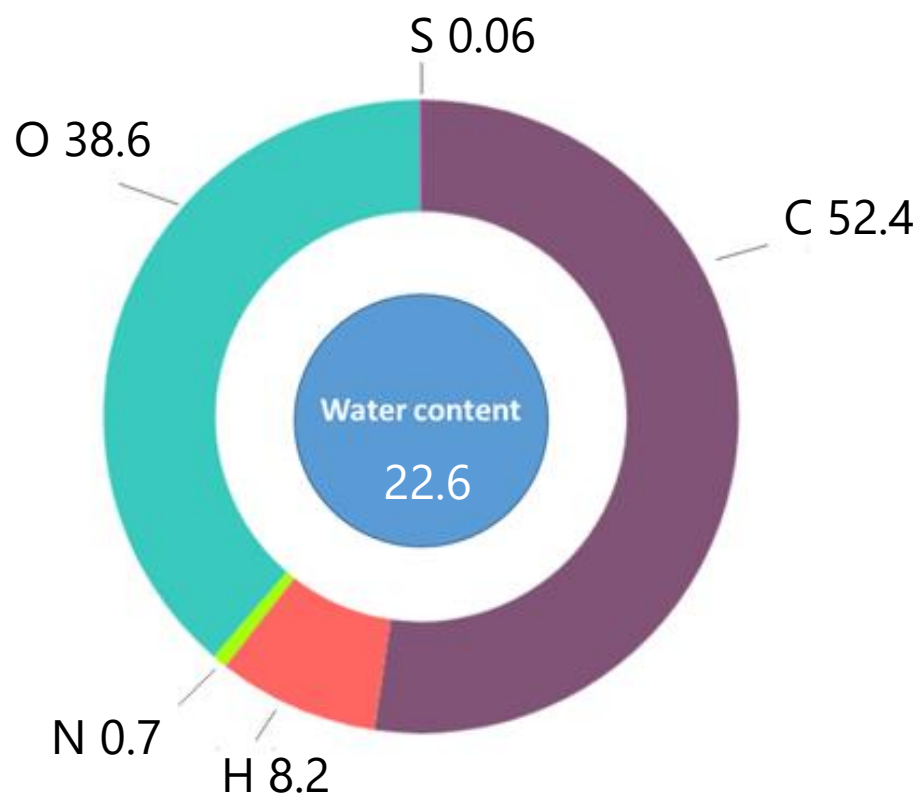
WHEAT/BARLEY STRAW BIO-OIL

Wheat/barley straw bio-oil

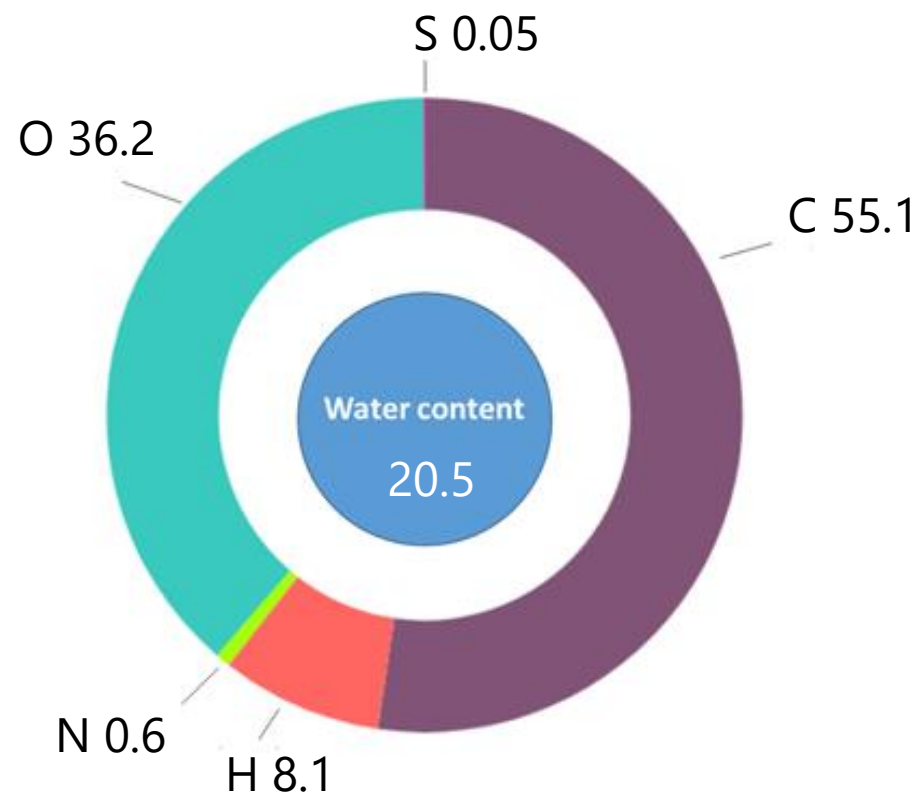


- T_{cond} 2-5 °C
- Aqueous phase yield = 27.9 wt%
- Bio-oil yield = 20.9 wt%

- T_{cond} 75 °C
- Bio-oil yield = 23.3 wt%



C
O
H₂O
Yield



- R** • Fixed-bed, co-current flow
- F** • Wheat/barley straw bio-oil
- C** • 340 °C, 40 bar, TOS 80 h, LHSV 1h⁻¹
- C** • Presulphided NiMoS/Al₂O₃

2-5 °C and 75 °C

Based on our previous experiments

S_{BET} : 86.5 m²·g⁻¹
3.9% Ni and 15% Mo
0.8-1.2 mm particle size





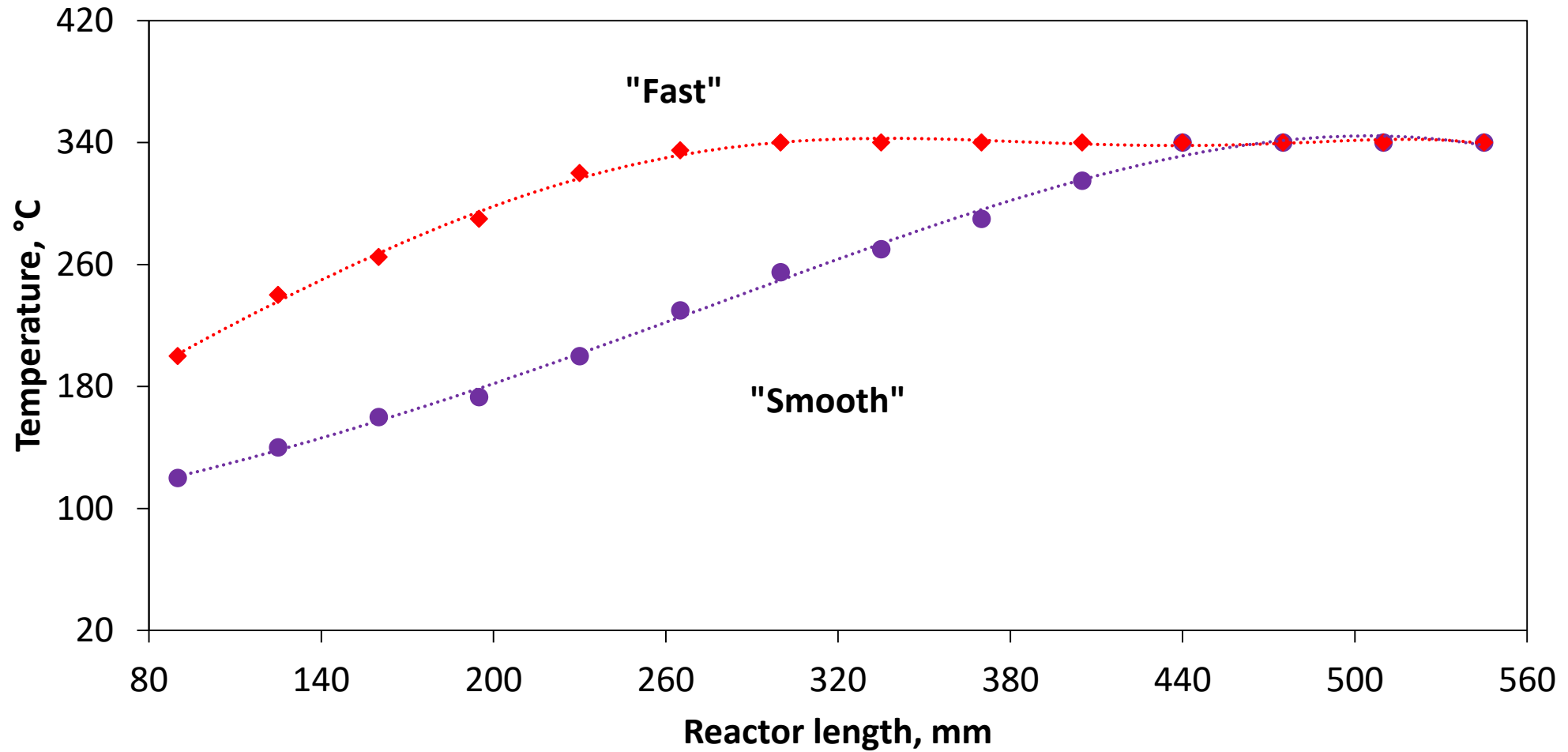
Hydrogenation of wheat/barley bio-oil 2-5 °C

Part 1: effect of thermoprofile



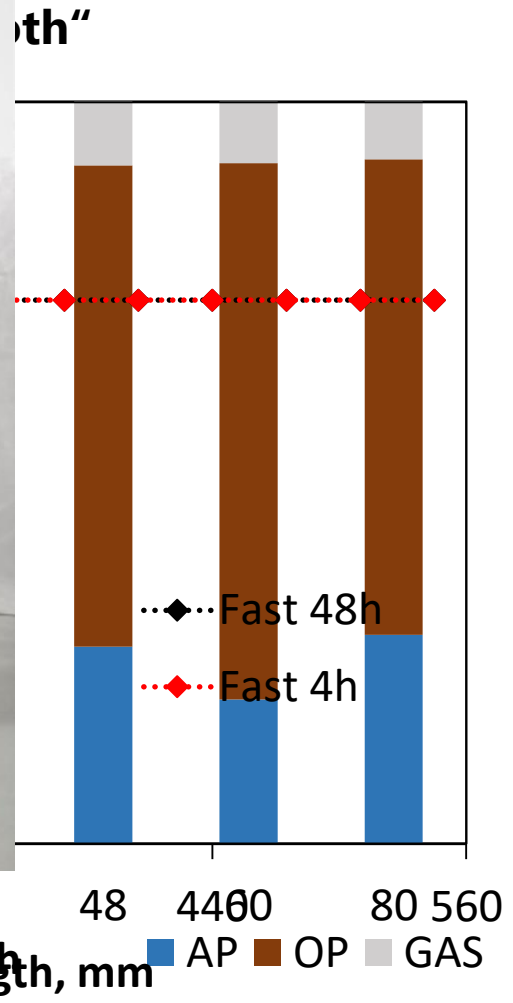
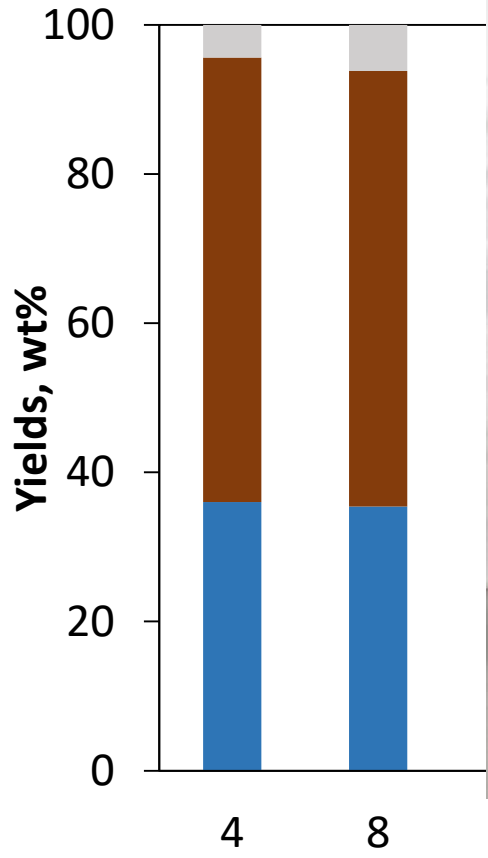
EFFECT OF TERMOPROFILE ON PRODUCTS QUALITY

Hydrogenation of bio-oil (2-5 °C) at two different thermoprofiles: fast increase to 340 °C and smooth increase to 340 °C



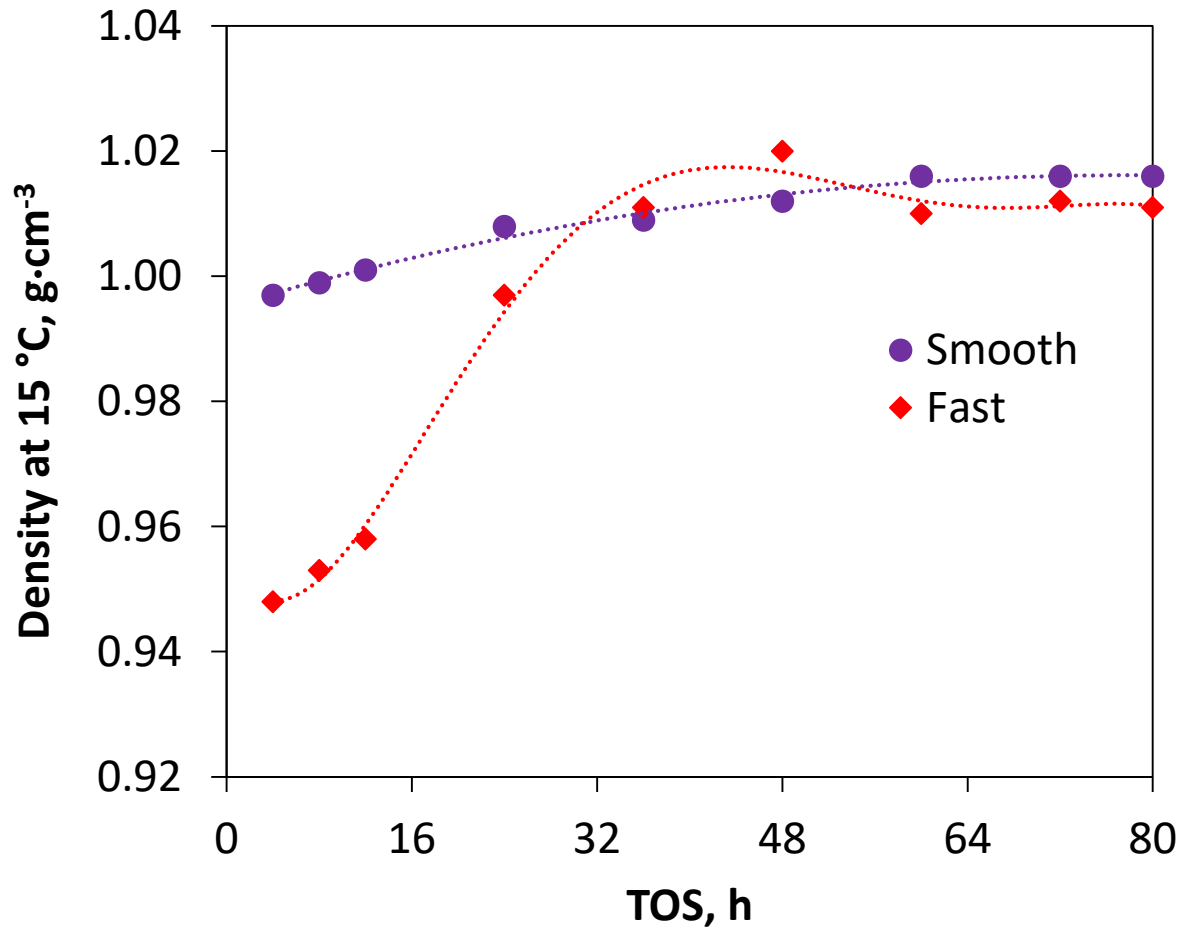
EFFECT OF TERMOPROFILE ON PRODUCTS QUALITY

All hydrogenated products were separated at two phases: organic and aqueous phase (OP and AP)

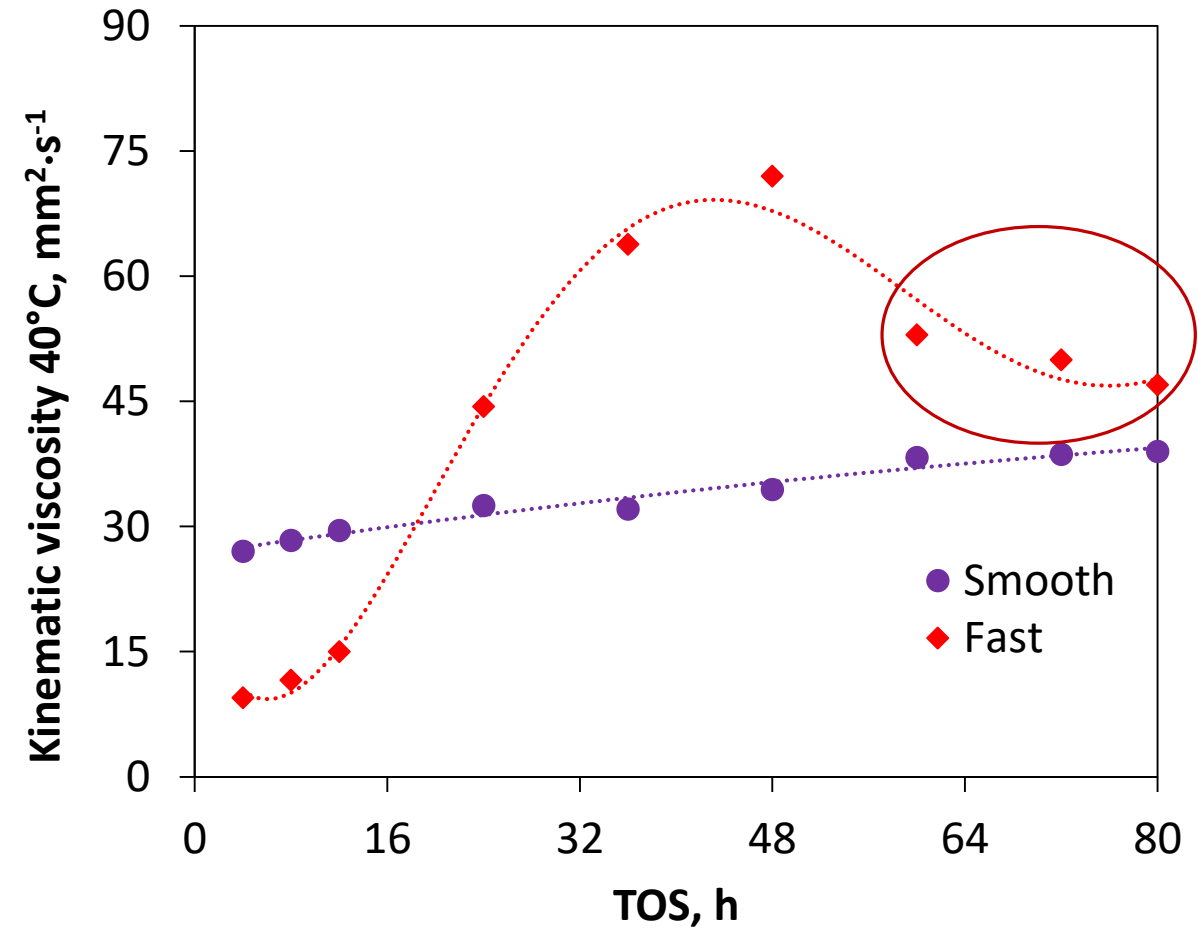


- High catalytic activity loss after 12 hours TOS leads to decrease of products properties („Fast“)

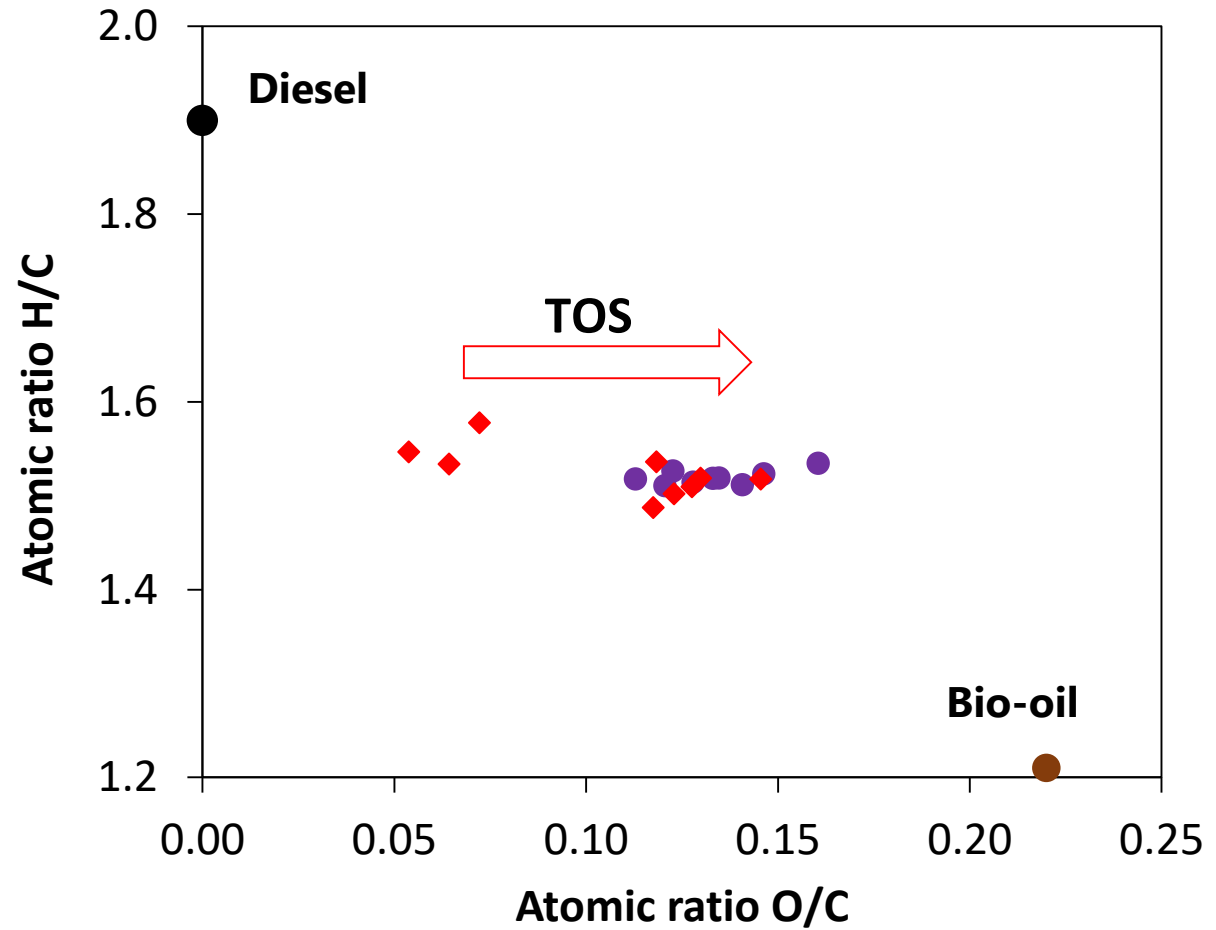
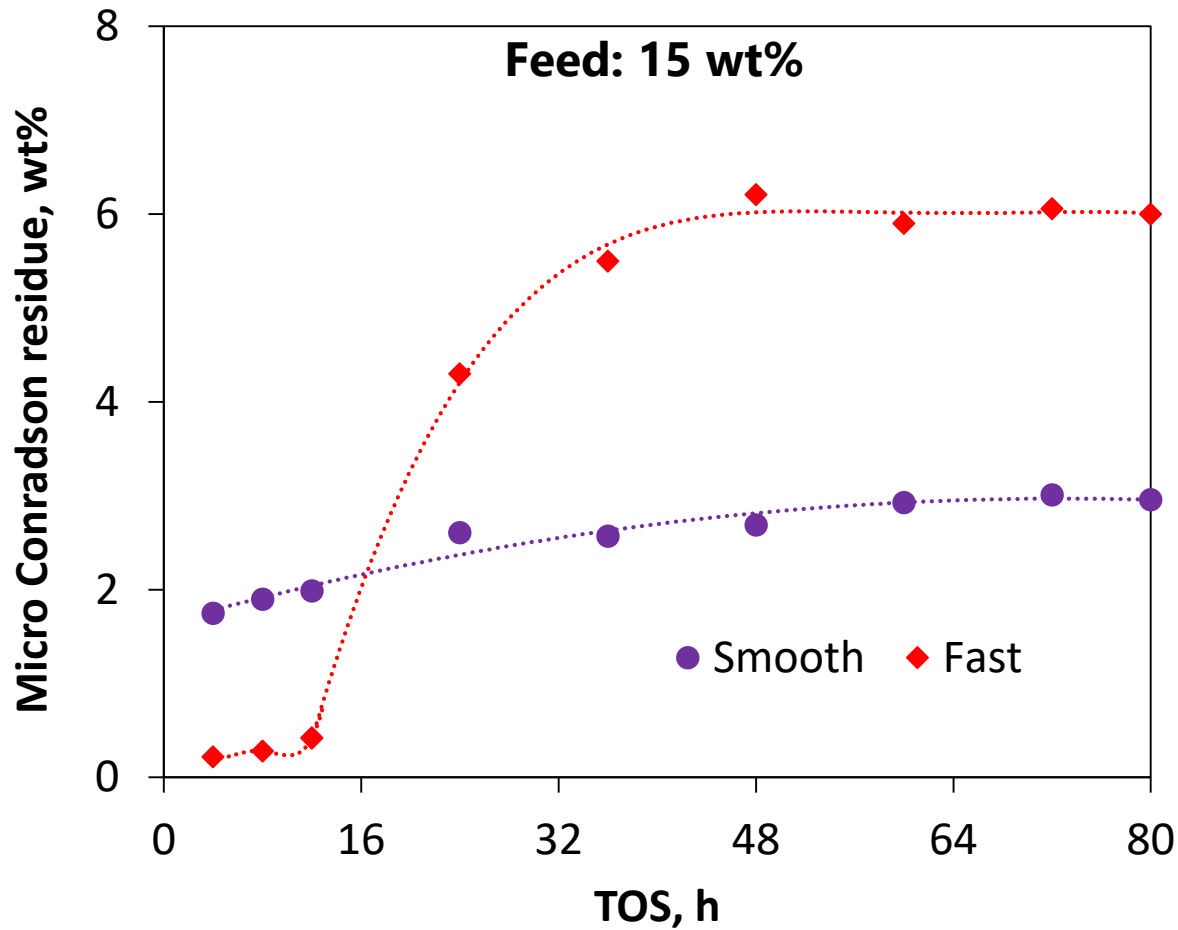
Feed: 1.13 g·cm⁻³



Feed: 123 mm²·s⁻¹

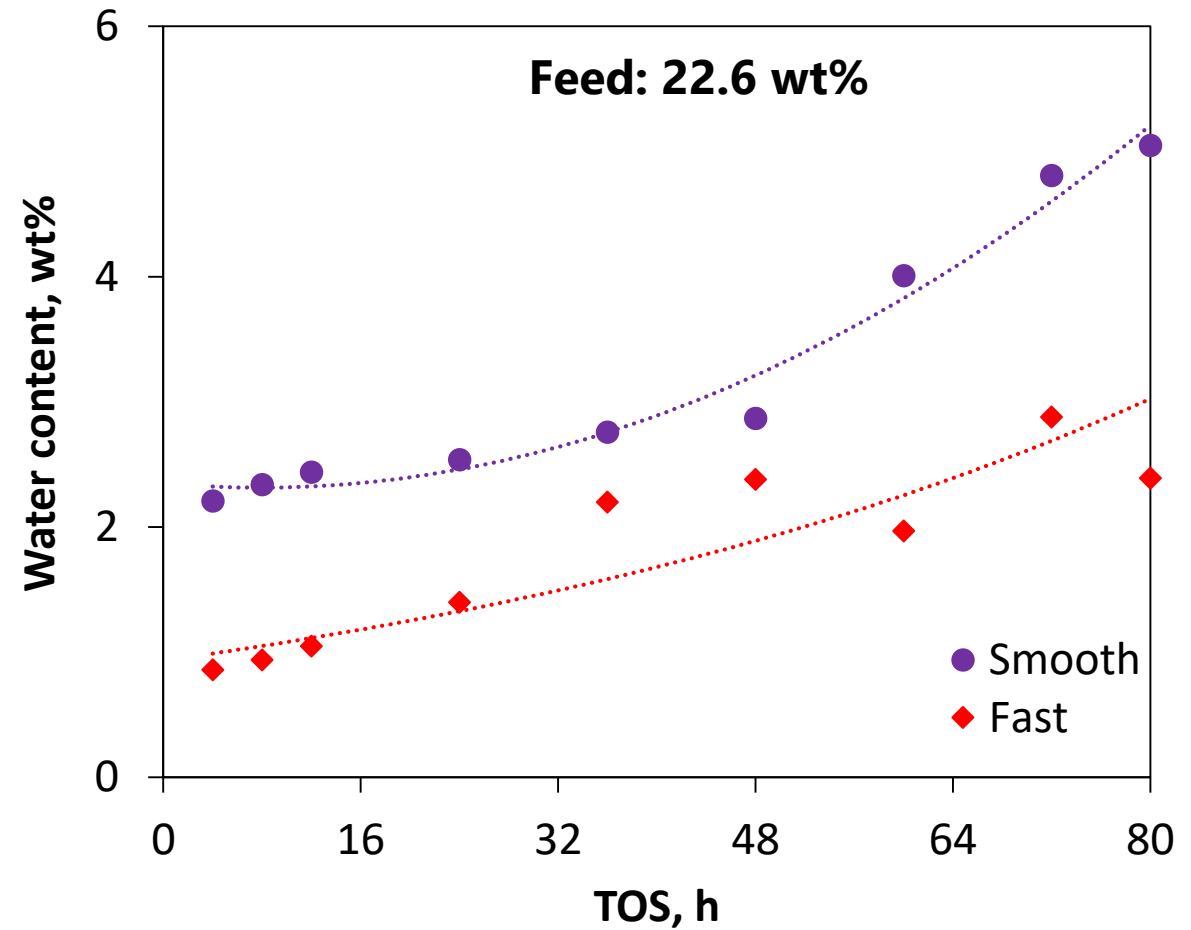
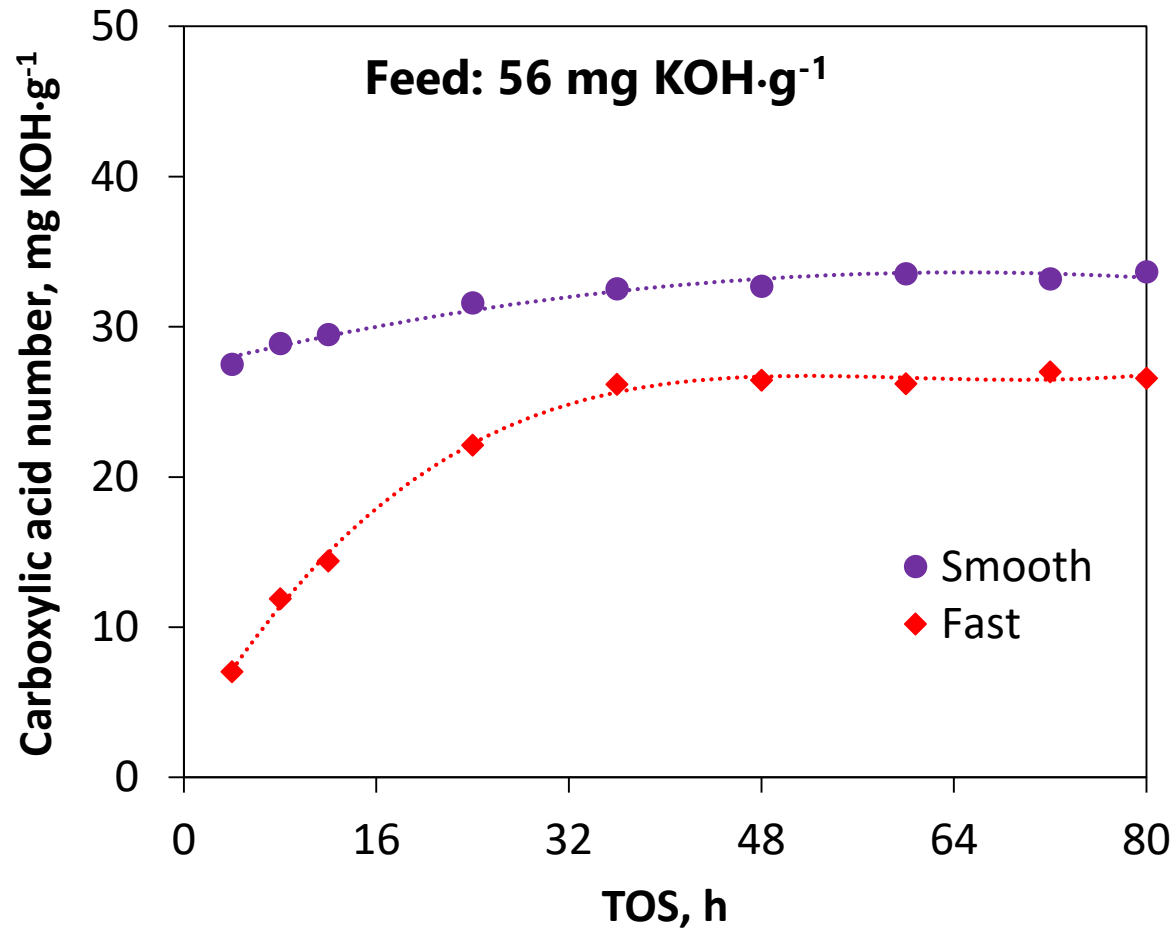


Significant increasing MCR value can be assumed as the most negative point of „Fast“ products even with other better properties

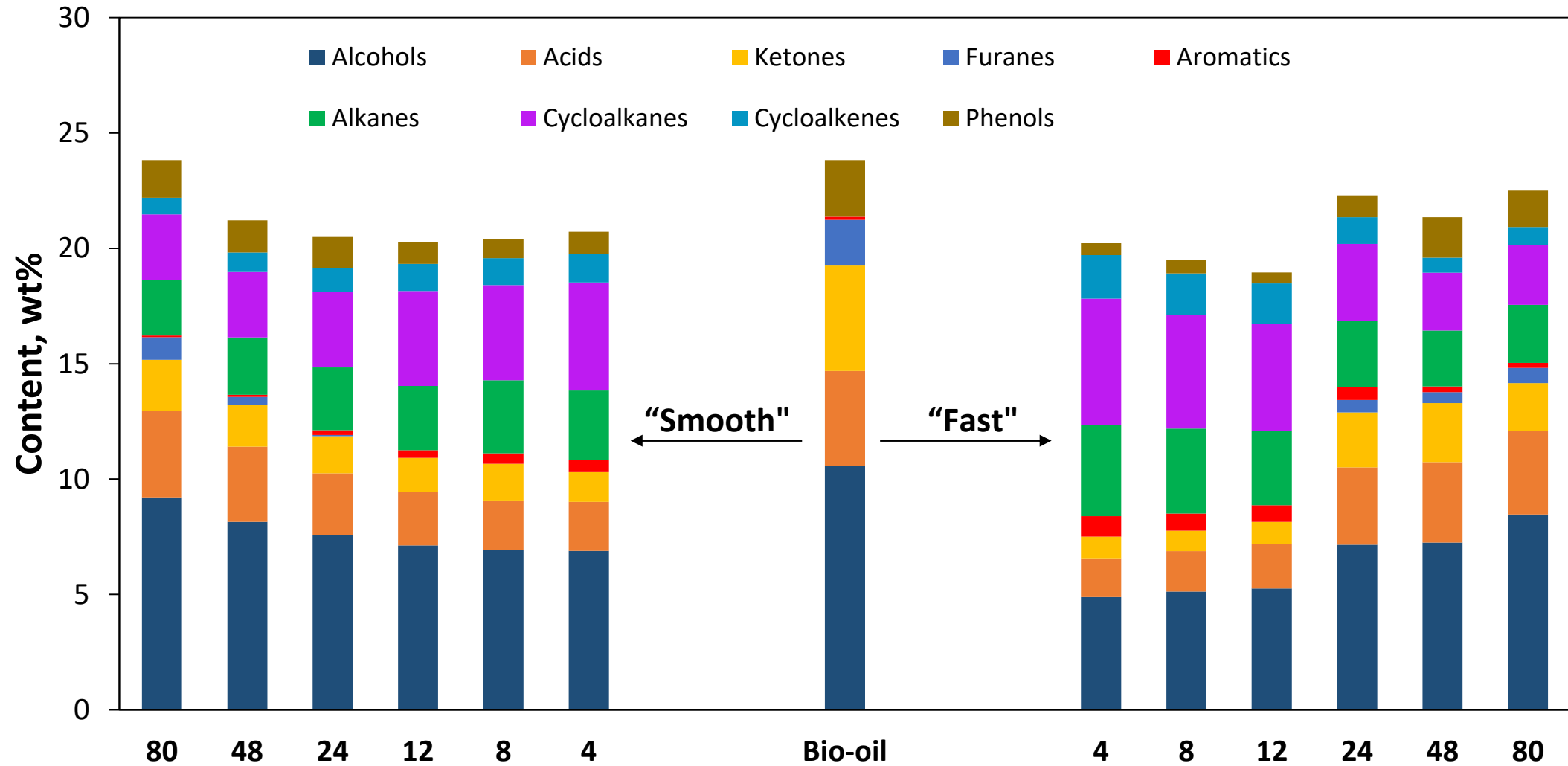




Corrosivity of bio-oil products can cause huge problems in refinery – should be blended with crude-oil/distillates



In all products were found alkanes, cycloalkanes/-alkenes that have not been observed in the raw bio-oil





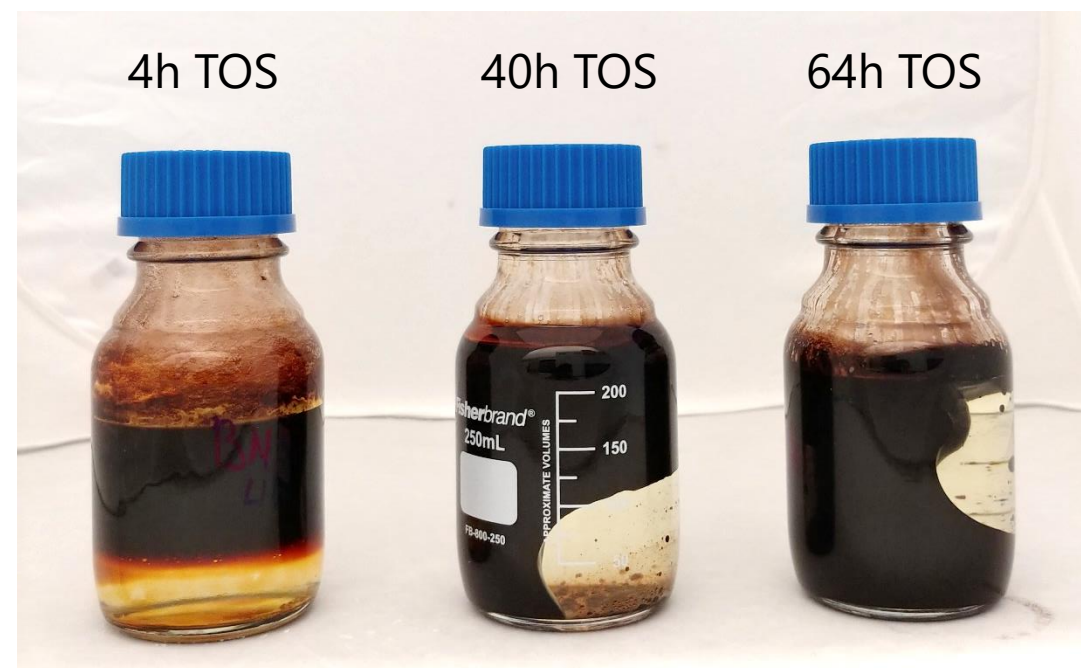
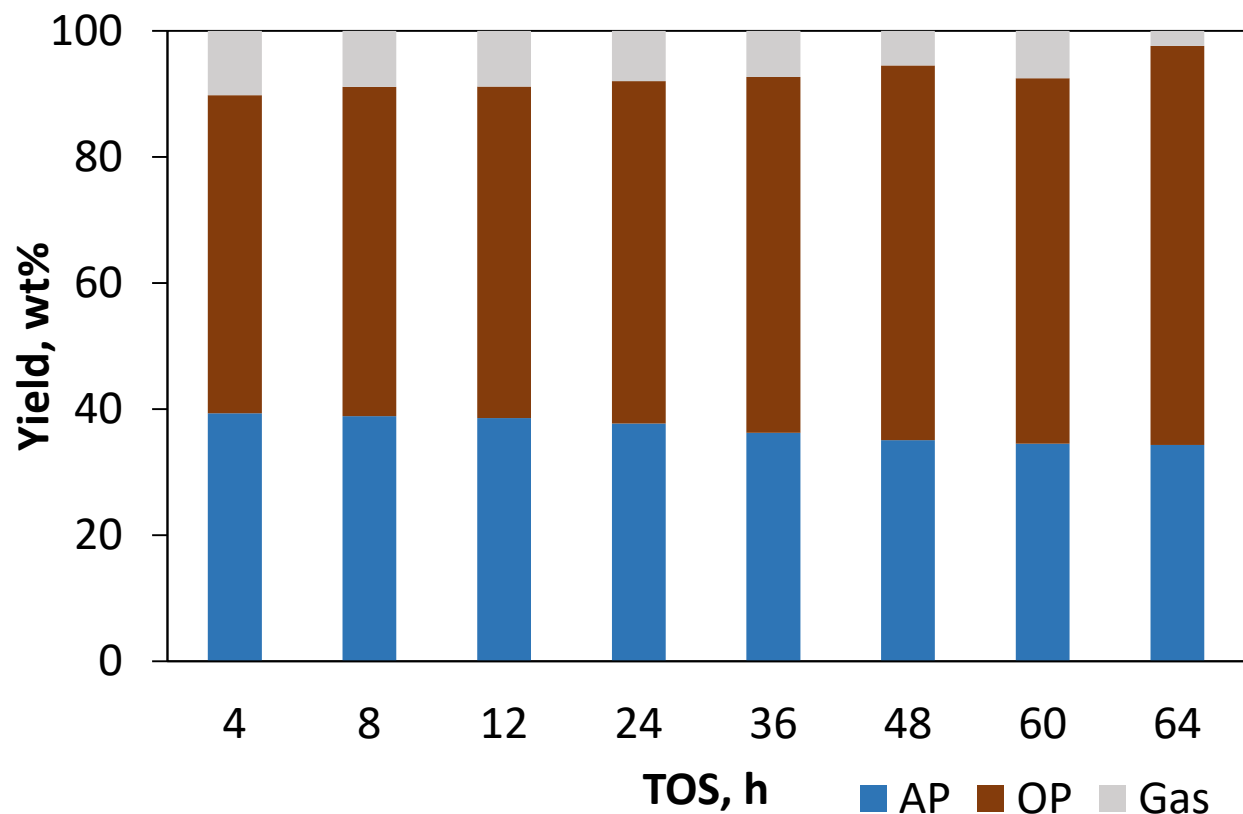
Hydrogenation of wheat/barley bio-oil 75 °C

Part 2: application of „smooth“ thermoprofile



HYDROGENATION OF STAGED CONDENSATED BIO-OIL

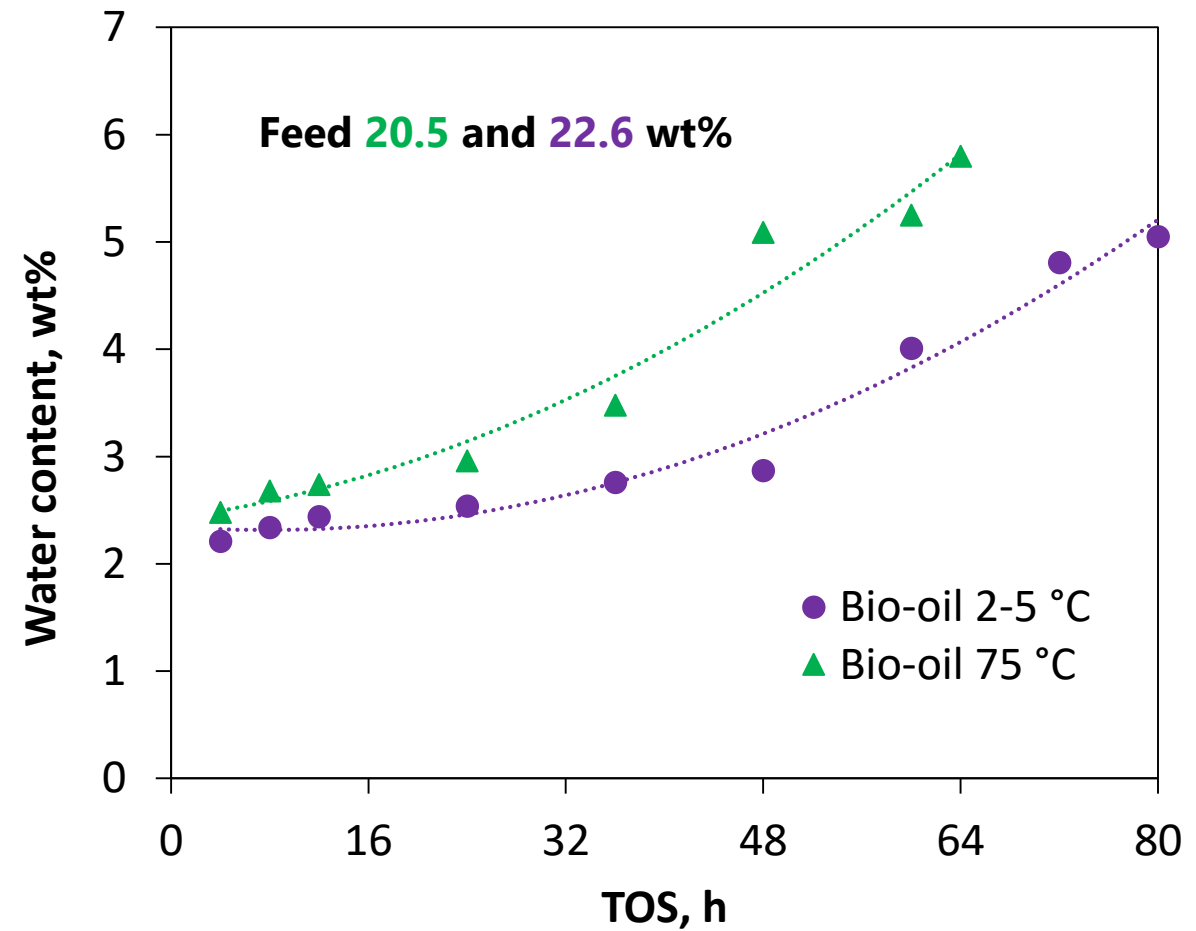
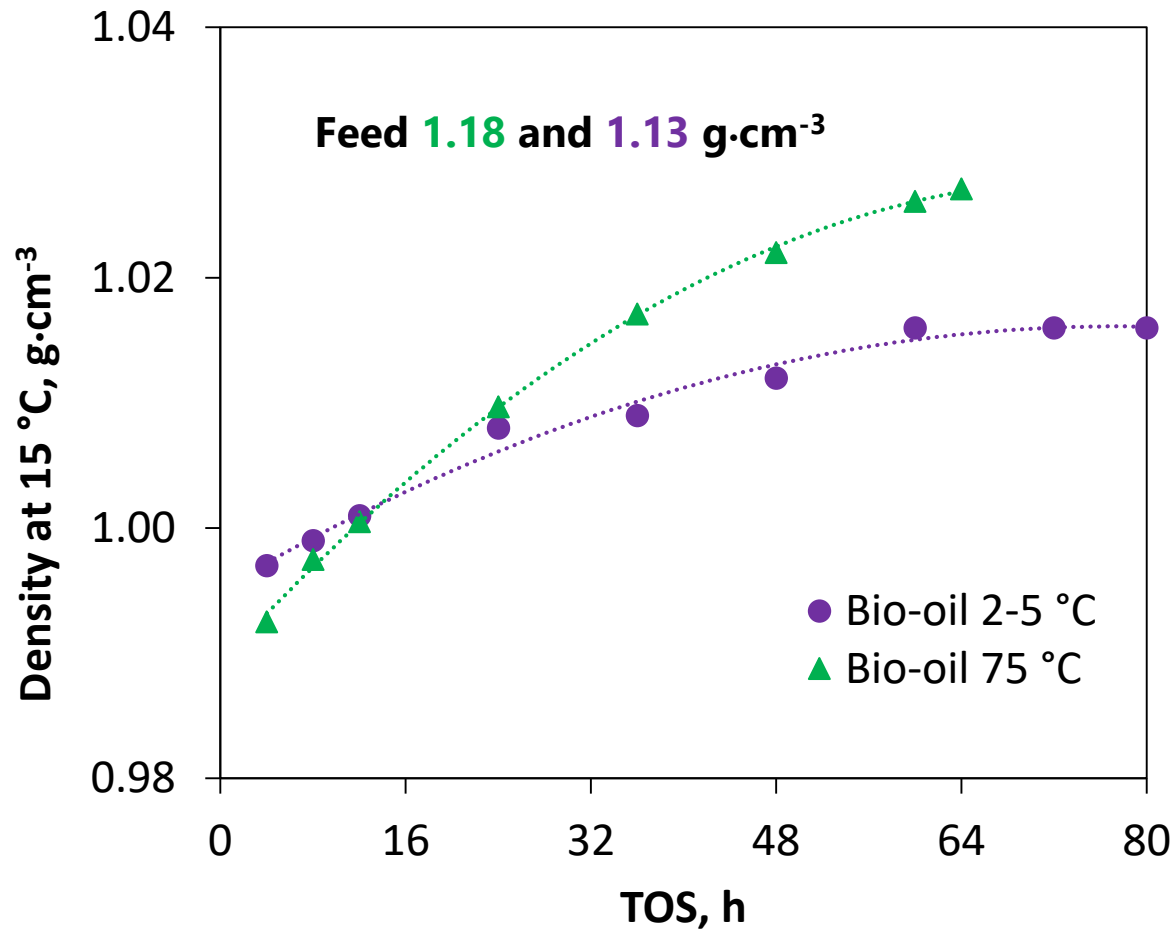
- „Smooth“ thermoprofile mode was applied for the hydrogenation of staged condensate bio-oil (75 °C) for 64 hours experiment
- After 40 h TOS organic phase density increased and all further products were not separated so well on two phases





HYDROGENATION OF STAGED CONDENSED BIO-OIL

- Higher loss of the catalytic activity during hydrogenation of staged condensed bio-oil was dominantly caused by higher CAN of feed ($80 \text{ mg KOH}\cdot\text{g}^{-1}$)



- Raw bio-oil is a complex mixture with unacceptable properties that should be upgraded to fulfil limits for transport fuels
- Hydrotreatment is a suitable technology for bio-oil upgrading in the fixed-bed reactor for producing low-cost petroleum-refinery-compatible feedstock
- Hydrotreatment thermoprofile play significant role in the upgrading process: „Smooth“ mode is preferred due to:
 - stable products properties
 - convenient unit operation
- Upgrading of bio-oil condensed at 2-5 °C gave more valuable products with similar properties at all TOS

Future plans: test two thermoprofiles for the hydrotreatment of miscanthus bio-oil (2-5 and 75 °C) and beechwood bio-oil



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