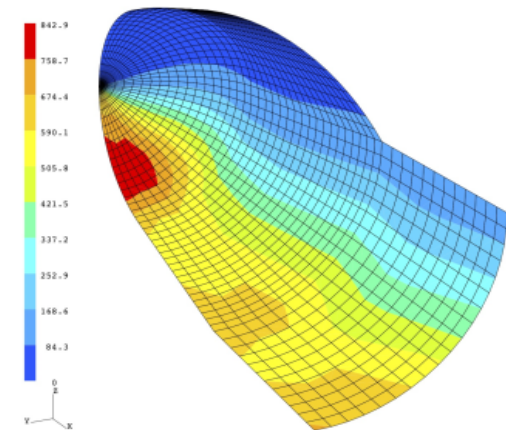




Inter-Code Calibration exercise series#2, Amaryllis results

Tom van Eekelen – LMS
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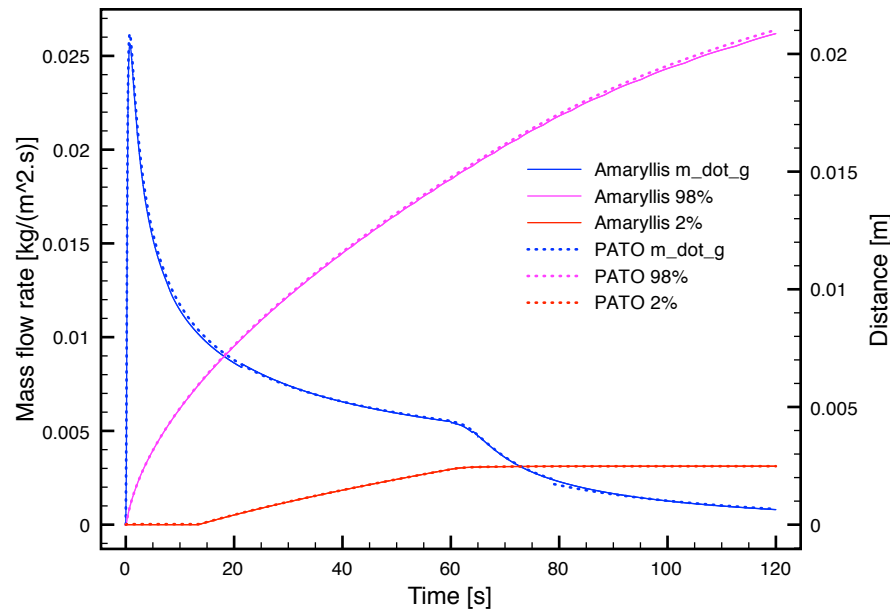
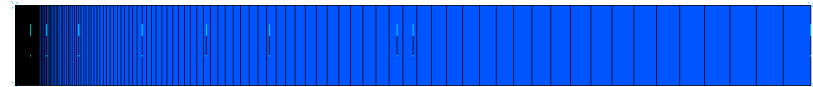
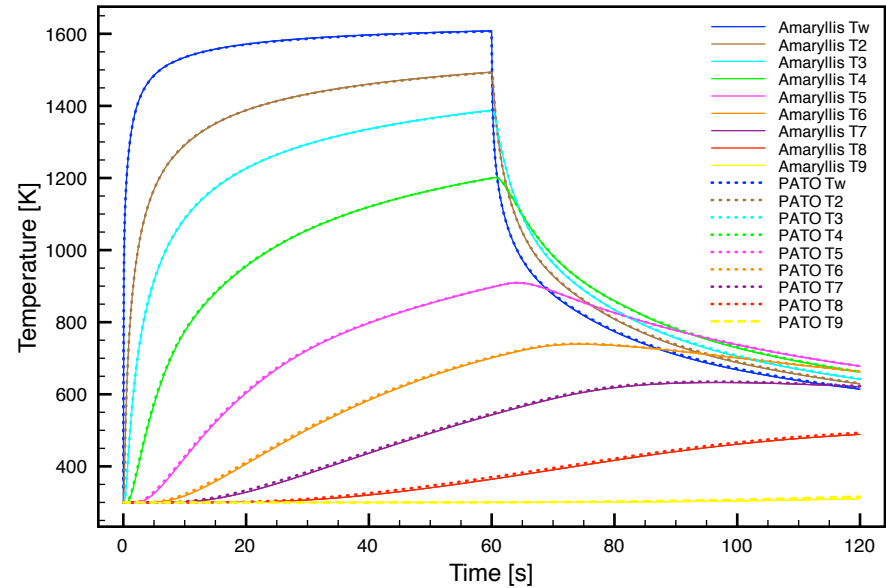
- 1D/Axis-symmetric/3D finite element code:
 - Non-linear structural analysis + thermal + charring-ablation code
 - Temperature (T), Pressure (P), density (ρ) and species density (α_i)
 - Mesh deformation due to ablation (multiple ablation zones)
 - Thermal contact algorithms for contact between:
 - Different ablation zones
 - Support structure and ablation zone
 - Multiple boundary condition types:
 - Convection (classical, enthalpy form)
 - flux
 - radiation
 - Ablation (imposed boundary condition):
 - Phase change
 - Chemical (explicit ablation speed or Bc' table; $Bc'=Bc'(T,P,Bg')$)
 - Mechanical (erosion; temperature and/or density dependent)
 - Fully coupled thermo-mechanical solution (char swell)



Amaryllis Test 2.1



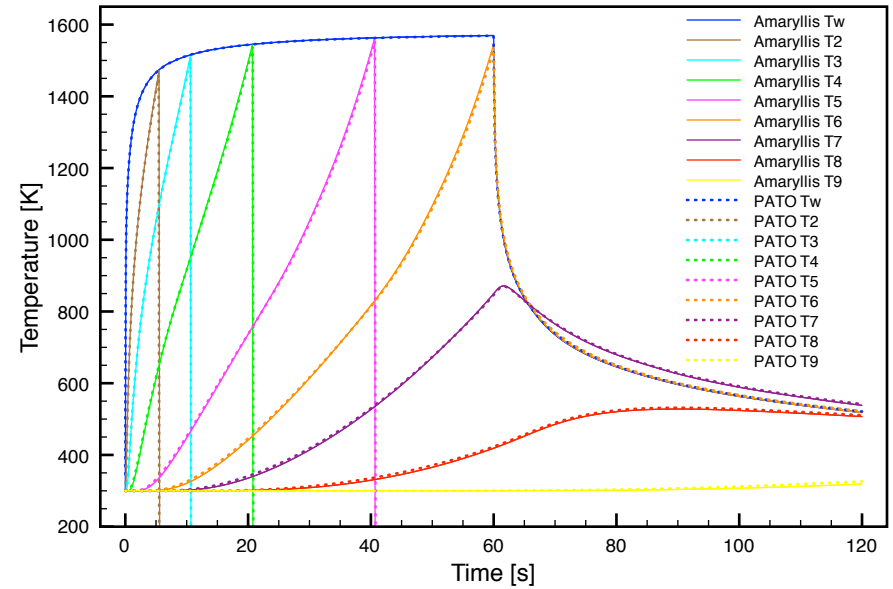
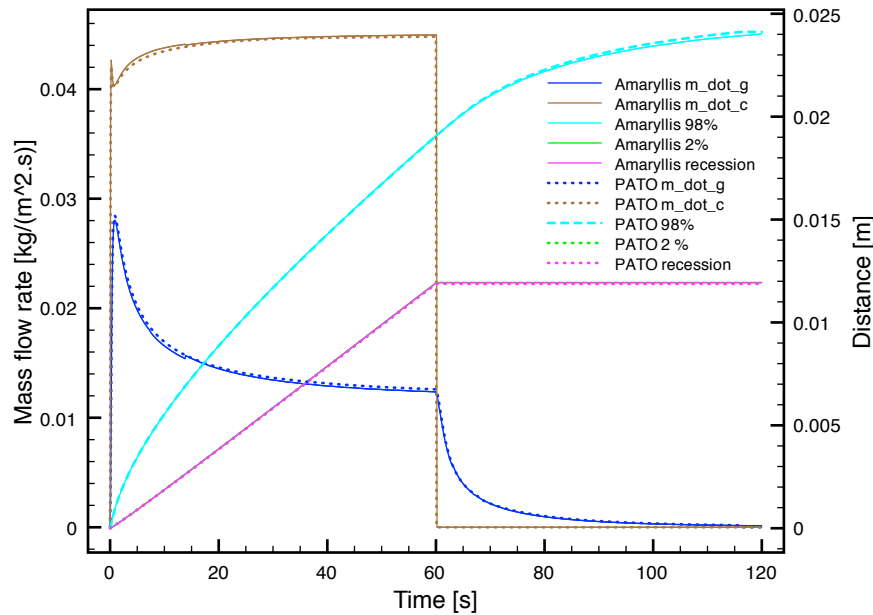
- Comparison Amaryllis:
 - PATO-PAM2 results are “identical”
 - No CMA/FIAT baseline available
- Fine mesh distribution is needed for the gas mass flow, not for temperatures



Amaryllis Test 2.2



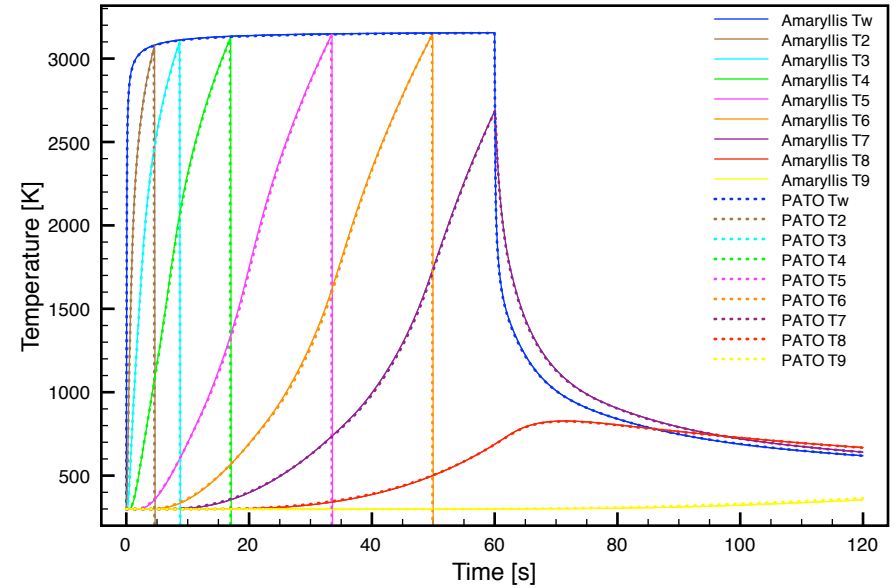
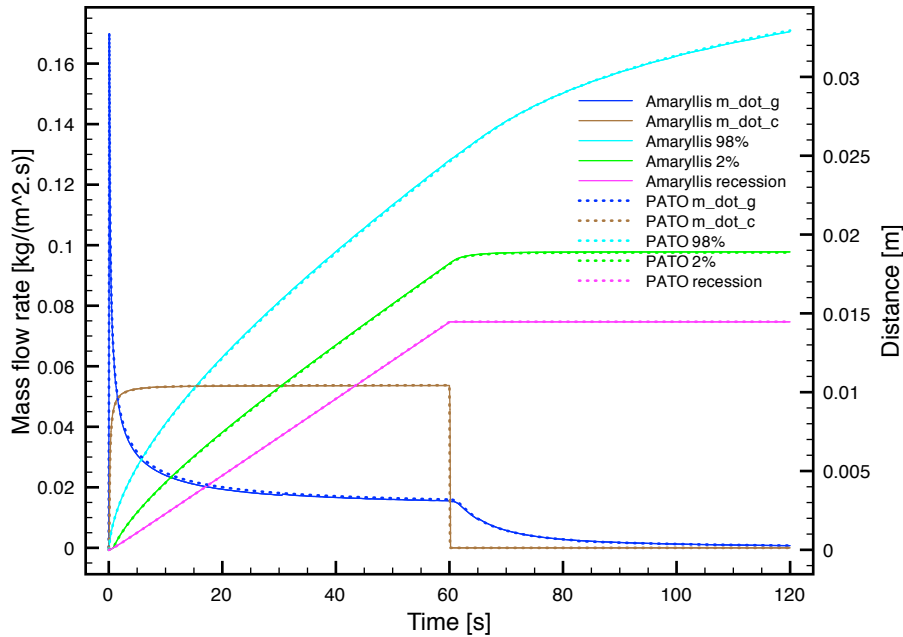
- Comparison Amaryllis:
 - PATO-PAM2 results are “identical”
 - No CMA/FIAT baseline available



Amaryllis Test 2.3



- Comparison Amaryllis:
 - PATO-PAM2 results are “identical”
 - No CMA/FIAT baseline available



- Arrhenius type charring equations

$$\dot{\rho} = - \sum \Delta \rho^i A_i \rho_v^{1-N_i} (\rho_v - \rho_c)^{N_i-1} (1 - \alpha_i)^{N_i} e^{-E_i/RT}$$

- Generalized densities $0 \leq \alpha_i \leq 1$

$$\rho = \rho_v - \sum \Delta \rho^i \alpha_i$$

- Mass balance equations

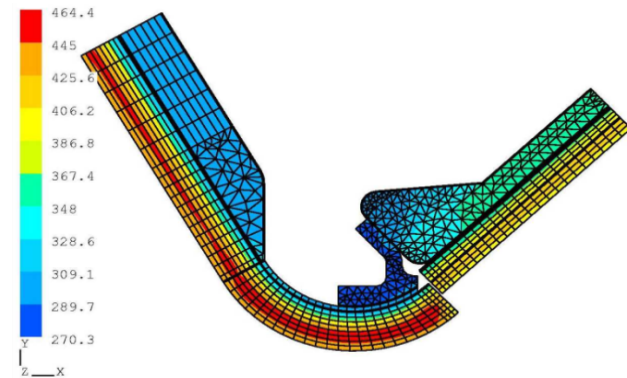
$$\nabla \cdot (K_p \nabla P) = \dot{\rho}$$

$$\dot{m}^g = -K_p \nabla P$$

- Heat balance equation

$$-\frac{\partial \rho}{\partial t} H_p + \rho c \frac{\partial T}{\partial t} = \nabla \cdot (\lambda \nabla T) - \dot{m}^g \cdot \nabla h^g$$

$$\bar{q} = -\lambda \cdot \nabla T$$



- Equivalence with the FIAT formulation.

- Interpolation
$$\alpha = \frac{\rho_v - \rho}{\rho_v - \rho_c}$$

- Capacity
$$\rho c = \rho c_v(T) - \alpha(\rho c_v(T) - \rho c_c(T))$$

- Pyrolysis heat
$$H_p = h^g - \frac{\rho_v h_v - \rho_c h_c}{\rho_v - \rho_c}$$

- Charring
$$\Delta \rho^i = \frac{\rho_{0_i} - \rho_{r_i}}{\sum (\rho_{0_i} - \rho_{r_i})} (\rho_v - \rho_c) \quad A_i = \frac{\Gamma_i (1 - \varphi) B_i \rho_{0_i}^{1-N_i} (\rho_{0_i} - \rho_{r_i})^{N_i}}{\Delta \rho^i \rho_v^{1-N_i} (\rho_v - \rho_c)^{N_i - 1}}$$

- Difference with the FIAT formulation

- Interpolation
 - conductivity
$$\lambda(T, \rho) = \lambda_v(T) - \alpha(\lambda_v(T) - \lambda_c(T))$$

- Mass balance
 - Perfect gas:
$$K_p = \frac{M^g \beta P}{\mu R T} \quad \beta = \beta_v \frac{\Omega}{\Omega_v} \quad \Omega = \Omega_v + (1 - \Omega_v) \frac{\rho_v - \rho}{\rho_v}$$

- K_p interpolation:
$$K_p(T, \rho) = K_{p_v}(T) - \alpha(K_{p_v}(T) - K_{p_c}(T))$$