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Anne M. Schumacher
University of Kentucky, annenschumacher@gmail.com

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Anne M. Schumacher, Student

Dr. Thomas M. Parris, Major Professor

Dr. Alan E. Fryar, Director of Graduate Studies

MODELING OF CO₂-WATER-ROCK INTERACTIONS
IN A MISSISSIPPIAN SANDSTONE RESERVOIR OF KENTUCKY

THESIS

A thesis submitted in partial fulfillment of the
requirements for the degree of Master of Science in the
Department of Earth and Environmental Sciences
at the University of Kentucky

By

Anne Marie Schumacher

Co- Directors: Dr. Thomas M. Parris, Adjunct Assistant Professor of Earth and
Environmental Sciences

and Dr. Alan E. Fryar, Associate Professor of Earth and Environmental Sciences

Lexington, Kentucky

2013

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ABSTRACT OF THESIS

MODELING OF CO₂-WATER-ROCK INTERACTIONS IN A MISSISSIPPIAN SANDSTONE RESERVOIR OF KENTUCKY

This study examined CO₂-water-rock interactions occurring during a carbon sequestration pilot test into a Mississippian oil reservoir in western Kentucky. New samples (n=62) and archived data, both collected from oil wells, were used to characterize the chemistry of formation waters from the Sugar Creek field in Hopkins County. In addition, core and cuttings samples (n=17) from the reservoir and overlying cap-rocks in, or near, the field were analyzed for bulk and clay mineralogy using X-ray diffraction. Electric logs were used to select sample intervals within the overlying cap-rocks and the center of the producing zones in the Jackson Sandstone. Using the water chemistry and mineralogic data as inputs, speciation and reaction path models were created using the Geochemist's Workbench software (GWB) to predict the distribution of aqueous species at equilibrium, evolution of fluid chemistry, and reservoir mineralogy as CO₂ was injected into the reservoir. Formation water was primarily Na-Cl. Reservoir rock was predominantly quartz. GWB simulations at the injection wells, mid-point fugacity and production wells indicated a sharp decrease in pH and increase in CO₂ (aq). Delta mineral mass plots showed net dissolution for injection stages and net precipitation for post-CO₂ injection. Important minerals were carbonates and alumino-silicates.

KEYWORDS: Carbon Sequestration, Modeling Subsurface Interactions, CO₂ Enhanced Oil Recovery, Geochemical Modeling, Carbon Capture and Storage

Anne M. Schumacher

April 2013

MODELING OF CO₂-WATER-ROCK INTERACTIONS IN A MISSISSIPPIAN
SANDSTONE RESERVOIR OF KENTUCKY

By

Anne Schumacher

Dr. Thomas M. Parris
Co-Director of Thesis

Dr. Alan E. Fryar
Co-Director of Thesis and
Director of Graduate Studies

April 2013

To Mom and Dad-

"The road to success is covered with parking spaces along the way."
Thanks for keeping me moving.

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Chapter 1: Introduction

Increases in amounts of atmospheric concentrations of greenhouse gases, especially carbon dioxide (CO₂), have raised concerns over the potential adverse effects to life on Earth. Combustion of fossil fuels (natural gas, oil, and coal) to meet human energy needs is a large source of carbon emissions. As the atmospheric concentration of CO₂ increases, solar radiation is trapped in the atmosphere and the Earth's surface temperature rises (IPCC, 2001). The temperature increase from rising atmospheric greenhouse gas concentrations is also of concern because it is likely to increase global sea level and change weather patterns worldwide (IPCC, 2005). Ongoing research has ensued to address global climate change and investigate a wide variety of stabilizing mechanisms (IPCC, 2001). Pacala and Socolow (2004) discuss numerous stabilizing mechanisms, including improved fuel economy, use of nuclear and wind power, reduced deforestation, and substituting natural gas for coal. Another potential mitigating mechanism is carbon capture and storage (CCS) in subsurface geologic reservoirs. Prospective CCS reservoirs include depleted oil and gas fields, deep saline/non-potable aquifers, un-mineable coal beds, organic-rich shales, and basalts. The CCS process proposes to capture CO₂ directly from anthropogenic sources (e.g. flue gas from coal-fired power plants) and inject it into geologic reservoirs for storage over time periods on the order of 10³ to 10⁴ years. Numerous pilot- and commercial- scale projects (e.g. Frio, Weyburn, In-Salah, Sleipner) have investigated the efficacy and challenges associated with CCS (Gale, 2002).

Though technically feasible in the appropriate geologic settings, CCS still faces technical, socio-economic, and regulatory challenges. One of the main challenges associated with CCS is to document the fate of injected CO₂ in the subsurface. This

monitoring, verification, and accounting (MVA) protocol is especially important because CO₂ is potentially chemically reactive with reservoir fluids (e.g. water, oil, and gas) and reservoir minerals.

1.1 Previous Work

The fate of injected CO₂ in storage reservoirs and the subsurface geochemical interactions in those reservoirs are being investigated through theoretical modeling, laboratory experiments, and field demonstrations. Enhanced oil recovery (EOR) is a mature technology within the oil industry and thus provides an extensive history in handling and injection of CO₂ (Melzer and Miller, 2007). In addition to previous use of CO₂ for EOR, the Burlington Allison Unit pilot project has been underway since 1996 to study CO₂ injection for enhanced methane recovery from deep coal seams (Gale and Freund, 2001). EOR projects have the benefit of providing economic return in addition to storing carbon. EOR projects, such as Sleipner West in the North Sea, Weyburn in Saskatchewan, and West Pearl in New Mexico, along with CO₂ injection projects in saline formations, such as Frio in Texas, have provided considerable insight into the physical and chemical behavior of CO₂ in the subsurface and implications for geological storage of CO₂ (Gale, 2002). General studies regarding issues surrounding the viability of CO₂ sequestration are abundant, including work by Bergman and Winter (1995), Holloway and van der Straaten (1995), Cook (1999), Gale (2002), Bachu (2000, 2002, 2003), Wildenborg and van der Meer (2002), Pacala and Socolow (2004), and many others.

The scientific community (e.g. Czernichowski-Lauriol *et al.*, 1996 and Gunter *et al.*, 1997) recognized the potential geochemical implications of long-term carbon sequestration as soon as the technology emerged. Since then, much progress has been made with respect to geochemical and solute transport modeling. Model evolution progressed from simple batch models assuming interactions only between CO₂, formation water, and rocks to complex three-dimensional flow models (Gaus *et al.*, 2008). Some recent papers of importance include Kharaka *et al.* (2006), who report gas-water-rock interactions within the Frio Formation following CO₂ injection; Zhang *et al.* (2009), who describe a case study from the Songliao Basin in China in which long-term variations of CO₂ trapped by different mechanisms within saline formations were analyzed; and Allen *et al.* (2005), who explain the significance of elevated pressures and salinities when modeling CO₂ sequestration within saline aquifers. Funded by agencies such as the Intergovernmental Panel on Climate Change (IPCC) and the United States Department of Energy (DOE), these studies represent a small part of a body of research, which has rapidly grown since the mid-1990's, examining the impacts and factors of using CCS as a climate-change mitigation option.

1.2 Statement of Purpose

Kentucky House Bill 1 (August 2007) provided funding and legislative mandate to conduct geologic carbon sequestration studies in saline aquifers, organic-rich shales, and oil and gas reservoirs. The legislation also called for an assessment of the application of CO₂ enhanced oil recovery (CO₂—EOR) in existing oil and gas reservoirs. EOR using CO₂ is viewed as a possible bridge mechanism to commercial-scale CCS in saline

aquifers because developed oil and gas reservoirs are typically geologically well characterized and the incremental oil production could produce revenue to offset some of the costs. Though CO₂-EOR is a successful and mature technology in many petroleum-bearing basins, it has not been extensively applied in the Illinois or Appalachian basins of Kentucky. Consequently, little is known about how CO₂ interacts with fluids and rock-forming minerals in reservoirs of this region. The geochemical interactions are important because they buffer pH and dictate how CO₂ is trapped in the reservoir through time. Additionally, the reactions could affect porosity and permeability of the reservoir and seal rocks through mineral precipitation and dissolution reactions.

The need to address the geochemical issues outlined above provides the motivation for the research in this thesis. The overall objective of this thesis is to assess potential geochemical reactions occurring between CO₂, water, and rock-forming minerals within the Jackson Sandstone, which is an oil-bearing Mississippian sandstone reservoir in western Kentucky and elsewhere in the Illinois Basin. The Sugar Creek oil field, Hopkins County, where the study reservoir is located is noteworthy because it was the site for a pilot CO₂ injection project administered by the Midwest Geologic Sequestration Consortium (<http://sequestration.org/>). The reaction modeling software, Geochemist's Workbench (GWB), is used to predict aqueous speciation and mineral saturation states in the reservoir before CO₂ injection and then changes in these parameters as CO₂ is injected into the oil reservoir for EOR and CO₂ storage. The reservoir aqueous and gas chemistry, mineralogy, and reservoir pressure and temperature data were collected before, during, and after CO₂ injection to serve as inputs into GWB.

The Sugar Creek pilot project provided the opportunity to develop a robust data set to examine potential reactions related to CO₂ injection using the GWB geochemical modeling software. Within the context of this pilot project, the goals of this study were to: 1) characterize the mineralogy of reservoir and seal rocks, 2) characterize the composition of aqueous reservoir fluids, 3) use GWB to characterize aqueous speciation and mineral saturation states of aqueous fluids before CO₂ injection, 4) use GWB to model possible reactions occurring between CO₂, aqueous formation fluids, and rock-forming minerals under different CO₂ concentrations, 5) compare reactions predicted by GWB with actual changes documented in the field, and 6) use GWB to simulate the effects of geochemical reactions on reservoir and seal porosity. Because many Mississippian oil reservoirs in western Kentucky and the Illinois Basin have similar temperature and pressure conditions and mineral compositions, the modeling results of this study should provide a valuable guide for examining reactions in future CO₂-EOR storage projects.

Chapter 2: Background

2.1 Geologic Background

Kentucky is divided into four major geologic provinces that include regional deformation and fault zones. The Illinois and Appalachian basins are the dominant features in western and eastern Kentucky, respectively. The Cincinnati Arch in central Kentucky separates the two basins, while the Mississippi Embayment covers the very western edge of the state (Figure 2.1; McDowell, 2001). Since the Sugar Creek oil field is located in western Kentucky, it will be helpful to look more closely at the geologic history of the Illinois basin, including stratigraphy, structure, and hydrodynamics.

2.1.1 Illinois Basin

As described by Swann (1967), the Illinois basin is an intracratonic basin filled with approximately three miles of shallow marine Paleozoic strata. The basin is a broad, elongate, north-south depression extending from northern Illinois and western Indiana southward through western Kentucky into northern Tennessee. Strata in the basin dip 1° (few feet per mile) toward the basin axis, which trends northwest-southeast. The majority of the Ordovician through Pennsylvanian strata in the basin consist of dolostone and smaller amounts of limestone, shale, sandstone, chert, anhydrite and coal. The Paleozoic strata are underlain by igneous and metamorphic basement rocks, which are approximately 1.3 billion years old (Swann, 1967).

Deformation in the basin is largely restricted to the LaSalle and DuQuoin-Louden anticlinal belts in Illinois, and the Rough Creek-Shawneetown fault zone, most of which is in Kentucky (Swann, 1967). These zones of deformation resulted from compressive

stresses created from collisions among South America, Africa and Laurentia during the Late Mississippian Appalachian orogeny (Swann, 1967; Kolata and Nelson, 1991).

2.1.2 Chesterian Lithology

Reservoir and seal rock samples in this study come from the Middle to Late Mississippian (Chesterian) section. Potter *et al.* (1958) did extensive work on the Chester sandstone depositional systems in the Illinois basin, and found that the sandstones were deposited under both fluvial and shallow-marine shelf conditions with sediment derived from a northeastern source beyond the margins of the basin, likely a large river system flowing southwest. Overall, about half of Chesterian series rocks are shale by volume with the remaining half split evenly between sandstone and limestone (Potter *et al.*, 1958). Each clastic unit within the series represents the advance of the Michigan River delta and subsequent filling of the shallow sea occupying the basin. Interruptions to sedimentation by major marine transgressions occurred six or seven times (Potter *et al.*, 1958; Swann, 1967). Basin subsidence coupled with a decreased sediment load resulted in these cyclical returns of the sea and limestone deposition (Swann, 1967).

The samples were collected from the Big Clifty Member of the Golconda Formation (Figure 2.2). The Big Clifty Sandstone Member is also called the Jackson sandstone (informal driller's term) and is henceforth referred to as the Jackson. Thickness of the Jackson can be 50 feet or more, and it is well-cemented, fine- to medium-grained, and is often cross-bedded (Fritz, 1967; Grabowski, 2001).

2.2 Hydrogeologic Background

Subsurface fluids include more than just freshwater; thus, it is important to know the composition of saline reservoirs and the movement of and interactions among various fluids (including gases or liquid hydrocarbons). Regional and local structures play significant roles in controlling fluid flow and composition through recharge and mixing. Other factors affecting flow include permeability, time, and density variations (Stueber *et al.*, 1993). The origin of fluid salinity, water-rock interactions, the pathways of fluid migration, and the timing of migration can all affect the composition of formation water as well. In this study, formation water refers to the aqueous reservoir fluids present in the Jackson. The fate of CO₂ injected into saline aquifers and many oil and gas fields will be affected by fluid flow direction and rate, and the composition of subsurface formation waters. Although there is no flow or transport component incorporated into this research, the basic concepts are necessary to understand subsurface interactions between reservoir fluids.

Sedimentary basins are ideal for geological storage of carbon because of the thick sequences of porous and permeable rocks, which are important in the transmission of fluids with varying densities (Gupta and Bair, 1997). Basins in tectonically quiescent areas (e.g. intracratonic and passive margin basins) are better suited to sequestration because of the decreased risk in fault hazards and potential reservoir leakage (Bachu, 2000). There is a close correlation between the flow regime of formation waters and both the age and type of sedimentary basin involved (Bachu, 2000). Flow in continental basins, such as the Illinois basin, is commonly controlled by topography, with fluids being recharged at high elevations and discharged at low elevations. Basin maturity, or

time, also plays a role in controlling flow direction. In mature, non-subsiding basins such as the Illinois Basin, flow is directed into the center of the basin (Gupta and Bair, 1997).

As Hanor (1994) explains, the composition of waters in sedimentary basins is affected by both chemical and physical processes, such as the basin-scale flow mechanism discussed above, which is an example of advection. Other transport processes that affect fluid composition include dispersion (mechanical mixing) and diffusion (mass movement driven by solute concentration gradients). Because the mixing of formation waters occurs fairly slowly and inefficiently, dispersion causes spatial and temporal variations in salinity (Hanor, 1994).

In addition to the natural driving forces (e.g. topographic relief), fluid composition can be affected by anthropogenic injection of fluids, such as waste disposal and EOR. For example, in this study, the operator at Sugar Creek mixed together formation waters of varying composition from different stratigraphic units (Pennsylvanian and Mississippian) as part of the water-flooding EOR plan. Formation-water composition can be also be modified after deposition by diagenetic reactions, including redox and acid-base reactions, mineral hydrolysis, and exchange with other fluid phases. Understanding mineral hydrolysis reactions, including the dissolution and precipitation of silicate and carbonate minerals, can increase solute concentrations in addition to affecting porosity in reservoirs. Additionally, formation waters in contact with oil within the reservoir can have elevated concentrations of organic acids, dissolved methane and bromide concentrations (Kharaka *et al.*, 1986). Notwithstanding the previously mentioned processes, fluid composition in many basins, including the Illinois, show a somewhat regular trend of increasing salinity with depth (Hanor, 1994).

2.3 Carbon Sequestration

According to the U.S. Department of Energy (DOE), carbon sequestration into geologic reservoirs is one of the most auspicious technologies (U.S. DOE, 1999, 2004) to help mitigate atmospheric concentration of CO₂, the main greenhouse gas, which has increased since the Industrial Revolution. Although much of the necessary scientific, technical, and industrial knowledge already exists largely because of experience gained in the oil and gas industry, commercial-scale implementation of carbon sequestration has been slow due to high costs and the need to accurately document the fate of CO₂ in the subsurface (Wildenborg and van der Meer, 2002; Bachu, 2003).

2.3.1 Storage Reservoirs

Assurance of environmental safety and project effectiveness requires that particular attention be given to the selection of appropriate storage reservoirs in order to minimize leakage. An ideal reservoir would have a large capacity in which to store CO₂ and be overlain by low porosity and permeability rocks that would block the upward migration of CO₂ (Wildenborg and van der Meer, 2002). Mature sedimentary basins that formed in mid-continental settings or on the edge of stable cratons are ideal for sequestration due to their stability and structure. Because of their geologic and technical maturity, these basins will likely have: (1) a well-documented geologic framework; (2) hydrocarbon reservoirs, if present, that are near depletion or abandonment; and (3) some of the infrastructure necessary for the transport and injection of CO₂ (IPCC, 2005).

Worldwide, reservoirs that are being investigated for carbon storage include: (1) deep saline formations, (2) depleted or abandoned oil and gas fields, (3) unmineable coal beds, (4) organic-rich shales, and (5) basalts (U.S. DOE, 1999, 2004; Greb and Harris,

2009). In Kentucky, saline formations, oil and gas fields, and organic rich shales are considered prospective, although the shale potential is more speculative (Parris *et al.*, 2010). Saline aquifers, which contain mostly non-potable water, have the greatest storage potential with an estimated capacity of 12 to 158 billion metric tons in the Illinois basin alone. Oil and gas reservoirs within the Illinois basin have an estimated storage volume of 140 to 440 million metric tons (U.S. DOE, 2012). However, the actual storage volume for CO₂ will be less than total reservoir pore volume because of reservoir heterogeneity, CO₂ buoyancy, and pore-level influences such as irreducible water saturation and capillary entry pressure (Bachu *et al.*, 2007).

Although they have less potential storage capacity than saline formations, a variety of factors make depleted oil and gas reservoirs excellent candidates for CO₂ sequestration. From a reservoir perspective, the most important attribute is the successful containment of hydrocarbons that were trapped for time periods in excess of the targeted 1,000 to 10,000 year time period for carbon storage. Moreover, throughout the life cycle of oil and gas development and production, the reservoirs were often extensively mapped and characterized, and engineering models were used in some fields to simulate subsurface fluid movement. Thus, the geometry and limits of the reservoir and trapping mechanisms are well documented. From a technology perspective, the methods used in the withdrawal of hydrocarbons, along with the injection and transportation of CO₂ in EOR projects, is directly transferable to sequestration projects (Wildenborg and van der Meer, 2002).

The use of CO₂ in a storage project to enhance oil and gas production can provide a revenue stream to offset injection costs, and thus the project can partly achieve both

economic and environmental goals (Wildenborg and van der Meer, 2002). However, it should be noted that combining these goals can be problematic for carbon sequestration goals because, for EOR to be economically viable, the field operator attempts to minimize the ratio of CO₂ injected relative to the incremental oil produced. Beyond economic considerations, infrastructure problems could occur in fields that have numerous abandoned wells that might be prone to leakage (IPCC, 2005).

2.3.2 CO₂ Properties

Knowledge of the physical and chemical properties of CO₂ is paramount to understanding potential fluid-rock-gas interactions once CO₂ is injected into the subsurface. CO₂ is a naturally occurring, colorless and odorless gas with an atmospheric concentration of approximately 392 parts per million (Voormeij and Simandl, 2002; Pacala and Socolow, 2004). When dissolved in water, CO₂ forms carbonic acid (H₂CO₃), which, as a weak acid, can affect both the chemical and physical properties of rocks in the reservoir and seal, and materials (e.g. cement) in injection and production wells (Gaus *et al.*, 2008). Other interactions will also occur elsewhere in the reservoir as CO₂ displaces formation fluids. For example, as CO₂ migrates as a free phase throughout the reservoir, it has the potential to cause a pressure perturbation depending on the rate of injection (Gaus, 2010).

The temperature and pressure of a prospective sequestration reservoir are important considerations because they will dictate the phase behavior of CO₂ and hence the storage efficiency. Generally, as temperature and pressure increase with depth, gaseous CO₂ becomes more liquid-like and liquid CO₂ becomes more gas-like. At the critical temperature of 87.8°F (31°C) and pressure of 1073 psi (75.11 bars or 7.38 MPa),

gaseous CO₂ is no longer distinguishable from liquid CO₂ and they form a single supercritical phase (Figure 2.3; IPCC, 2005; Greb and Harris, 2009). Formation of the supercritical phase is important because the density of the CO₂ increases significantly, which allows more CO₂ to be stored in a given volume (Figure 2.4; IPCC, 2005). Under hydrostatic conditions and a geothermal gradient of 25°C/km, the transition to supercritical CO₂ in many sedimentary basins occurs at depths of 800 to 1000 meters (Voormeij and Simandl, 2002; IPCC, 2005).

Temperature, pressure and salinity also affect the solubility of CO₂ in water. For a water with a given solute composition, the solubility of CO₂ increases with increasing pressure. On the other hand, temperature increase in the same water will decrease CO₂ solubility (Figure 2.5; Carr *et al.*, 2003). The corollary to this behavior is that dissolution of CO₂ in water occurs more readily in sedimentary basins that have low geothermal gradients and pressures above hydrostatic. Finally, increasing salinity will decrease CO₂ solubility because of the decrease in water activity (Figure 2.6; Carr *et al.*, 2003).

2.3.3 Storage Mechanisms and Potential Reactions

Effectively storing CO₂ in geologic formations depends on a combination of physical and geochemical trapping mechanisms that have differing degrees of permanency and storage security (Figure 2.7; Bachu and Adams, 2003; IPCC, 2005). The initial principal means of storage is physical trapping of single-phase CO₂ in stratigraphic or structural traps. Because CO₂ is less dense, it will displace formation water upon injection into the storage reservoir and migrate buoyantly upwards. Effective physical trapping will depend on having thick, low-permeability formations, such as shale or salt beds (stratigraphic traps), and/or folded rocks (structural traps) to act as upward

migration barriers. Hydrodynamic trapping can be extremely effective in saline formations that do not have a closed trap but have long fluid-transport times and distances (IPCC, 2005). In cases where there is an immense distance between the deep injection point and the end of the confining layer, the CO₂ and fluid can be trapped for millions of years (Bachu *et al.*, 1994). This is residual trapping, which refers to retention of CO₂ as an immobile phase in pore space within the storage reservoir. The injected CO₂ forms a plume that spreads vertically and laterally until it is trapped at residual CO₂ saturation (residual trapping), in a local structure, or below a sealing formation.

Another trapping mechanism is solubility trapping in which injected CO₂ dissolves into formation waters. The dissolution forms carbonic acid (H₂CO₃) that subsequently dissociates, resulting in a lowering of pH. The pH response to CO₂ injection can be quick as the dissolution and first dissociation reactions are relatively rapid (Cotton and Wilkinson, 1976; Kharaka *et al.*, 2006). Once CO₂ is dissolved in the formation water it is no longer buoyant, and migration as a discrete phase is no longer an issue. The final and most secure trapping mechanism is mineral trapping. This occurs when HCO₃⁻ or CO₃⁻ produced from the reactions above, for example, combines with cations (e.g. Ca²⁺, Mg²⁺, Fe²⁺) to form carbonate minerals and is stored in the solid phase (Gunter *et al.*, 1993; IPCC, 2005; Zerai, 2006).

2.3.4 History of Enhanced Oil Recovery (EOR) in Kentucky

The earliest history of enhanced oil recovery in Kentucky consisted of using natural gas to repressurize reservoirs with the intention of keeping the mobility of the oil in the reservoir from decreasing. The repressurization technique was used by the Petroleum Exploration Company and Ashland Oil Company in the Big Sinking oil field

(1926), Keaton-Mazie oil field (1929), and Haynesville oil pool (1935). By the 1950's water-flooding became the most popular technique used for EOR, and it has remained widely employed in Kentucky to maintain reservoir pressure and sweep oil from the reservoir (Duchscherer, 1965; Miller and Hamilton-Smith, 1998).

Although enhanced oil recovery using CO₂ has been used extensively in west Texas and Wyoming, the CO₂-EOR history in Kentucky is limited to several small-scale projects (Duchscherer, 1965; Miller, 1990; Bardon *et al.*, 1991; Miller *et al.*, 1994; Miller and Hamilton-Smith, 1998). These are single-well cyclic projects in which CO₂ is injected into a single well and then the same well is produced at a later date after a shut-in or “soak” period. During the shut-in period, CO₂ interacts with the oil, reducing its viscosity and making it more mobile in the reservoir. The CO₂-oil interaction is limited because Kentucky oil reservoirs often have reservoir pressures at or below the hydrostatic gradient and the low pressure produces immiscibility between the CO₂ and oil. The reduced recovery efficiency associated with immiscible CO₂-EOR coupled with the historical absence of an affordable and readily available source of CO₂ have limited its use for EOR in Kentucky (Melzer and Miller, 2007).

2.4 Study Area: Sugar Creek Field

The Sugar Creek field was discovered in 1964 in Hopkins County, Kentucky (Figure 2.8). Before injection of CO₂, primary and secondary oil production from the Jackson equaled 895,575 barrels of oil, which represents 33% of the estimated 2.7 million barrels of original-oil-in-place (Gallagher [field operator], unpublished). The oil at Sugar Creek has a gravity of 37 API, is stratigraphically trapped due to a pinch-out of the

Jackson (Figure 2.9), and the primary reservoir drive mechanism is a solution gas drive. Reservoir thickness ranges from 10 to 15 feet, and average porosity and permeability are 16.7% and 15.9 millidarcies, respectively. Average reservoir depth equals 1870 ft. The Sugar Creek CO₂-EOR pilot project was part of a broader pilot program administered by the Midwest Geological Sequestration Consortium and sponsored by the DOE. Goals of the pilot program were to inject CO₂ into several representative oil fields in the Illinois basin, document the influence on oil production, estimate the amount of CO₂ that remained in the reservoir over the course of the project (i.e. CO₂ storage), ascertain the viability of CO₂-EOR, and develop a set of best practices for CO₂-EOR.

Beginning in 1993 and prior to CO₂ injection, the operator implemented a water-flood project as a transition from primary production to secondary recovery. Water for the flood project was taken from a shallow Pennsylvanian sandstone aquifer. This Pennsylvanian formation water is significantly less saline than the formation water in the Jackson and injection has produced variable dilution of the latter. Therefore, Jackson formation water samples from Sugar Creek represent the mixing of Pennsylvanian and Mississippian formation waters. Wilbur-Todd #3 (WT3) was the source of the dilute shallow Pennsylvanian formation water used in the water flood.

From May 11, 2009, to May 13, 2010, 7,268 tons of CO₂ were injected into the Jackson through a central injection well, the Ross-Gentry #5 (RG5), at a rate of 20 to 30 tons per day. Pre-injection reservoir pressure and temperature at RG5 were 700 psi (49 bars) and 28°C, respectively. During CO₂ injection at RG5, pressure increased an additional 1200 psi (84 bars) so that total reservoir pressure equaled 1900 psi (133 bars). Surrounding the RG5 are seven producing wells: Pressley-Hart #1 (PH1), Ross-Gentry #1

(RG1), Ross-Gentry #2 (RG2), Ross-Gentry #3 (RG3), Ross-Gentry #4 (RG4), Wilbur-Todd #4 (WT4), and Wilbur-Todd #9 (WT9). Before, during, and after CO₂ injection, the production wells, in contrast, were pumped at a sufficiently high rate that reservoir pressure equaled approximately 30 psi (2 bars). The horizontal distance between RG5 and production wells ranges from 500 to 1,500 feet. Consequently, a significant horizontal pressure gradient developed in the reservoir where production wells were close to the injection well.

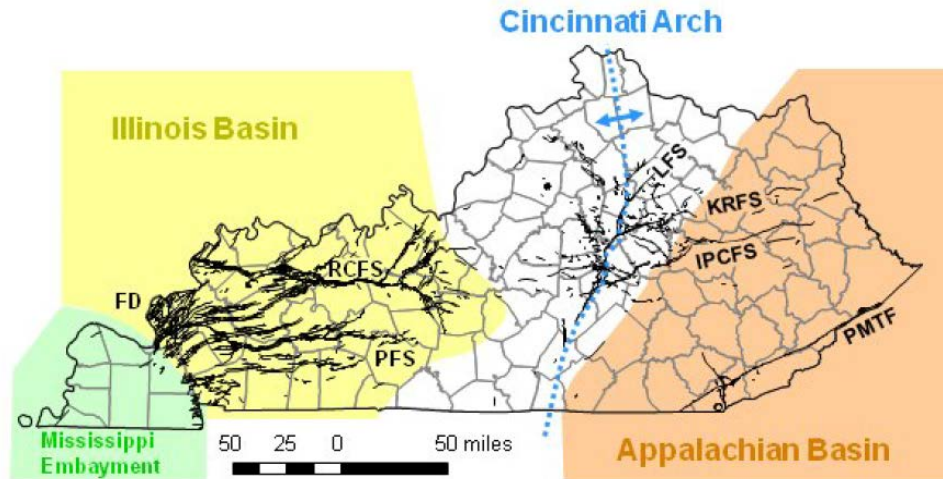


Figure 2.1 Structural setting of Kentucky with faults abbreviated as follows: FD- Fluorspar District, RCFS- Rough Creek Fault System, PFS- Pennyroyal Fault System, LFS- Lexington Fault System, KRFS- Kentucky River Fault System, IPCFS- Irvine-Paint Creek Fault System, and PMTF- Pine Mountain Thrust Fault (Greb and Solis, 2009).

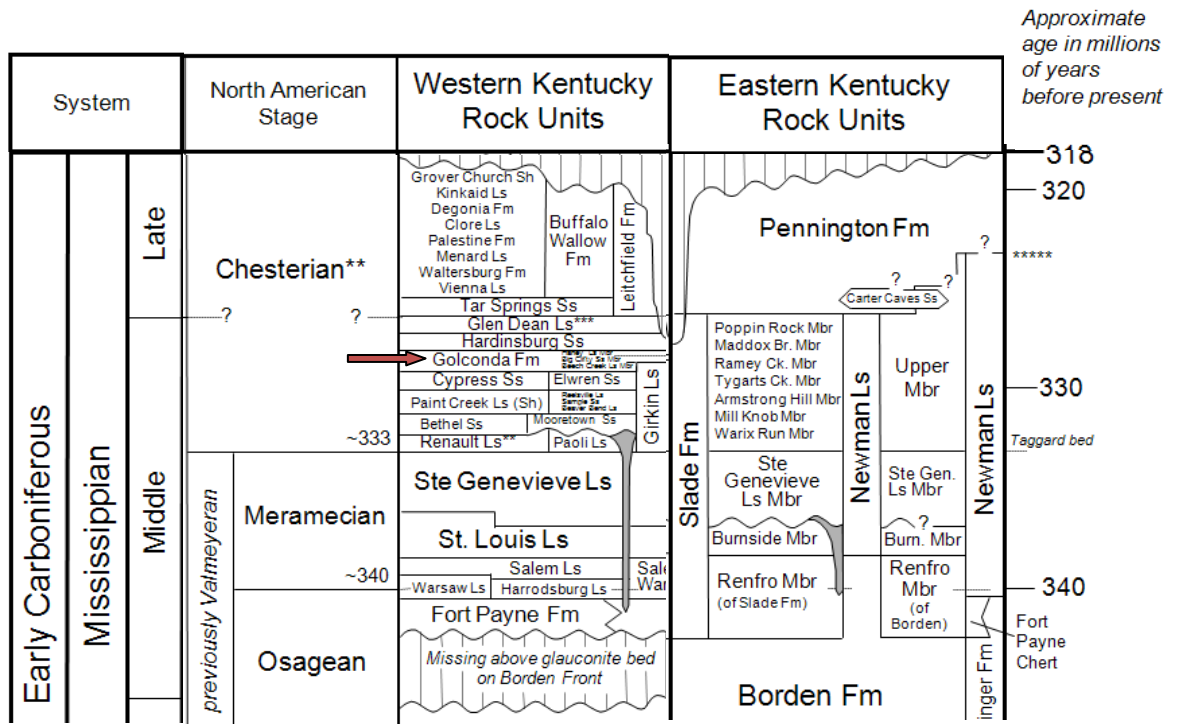


Figure 2.2 Mississippian rock units in eastern and western Kentucky. Bold arrow points to the Golconda Formation that contains the Jackson (Modified from S. Greb, unpublished).

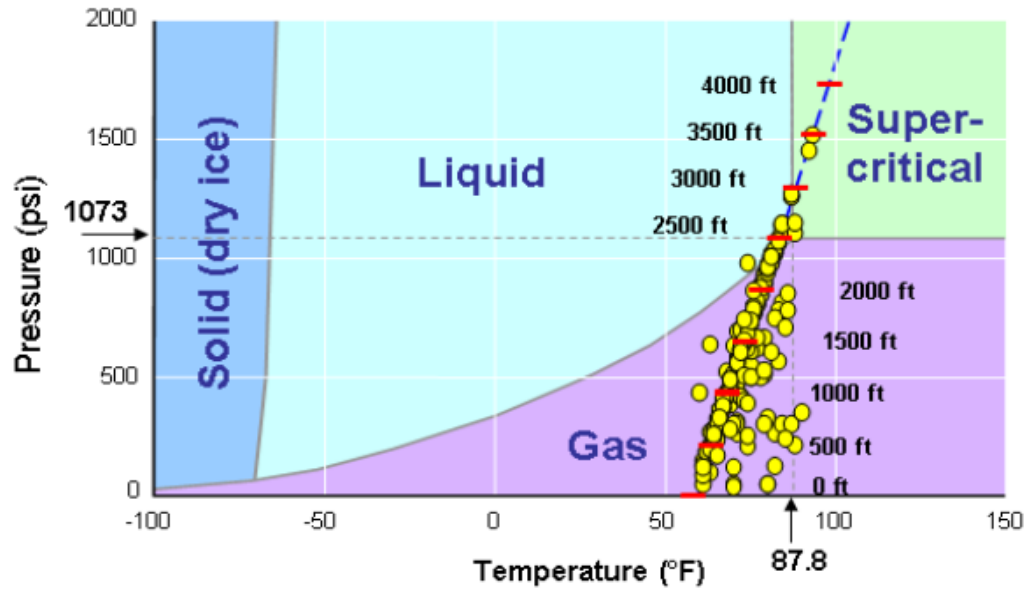


Figure 2.3 Range of temperatures and pressures where CO₂ phases are stable. Circles represent temperatures and pressures for Kentucky oil and gas wells at increasing depths (Greb and Harris, 2009; data compiled by B. C. Nuttall).

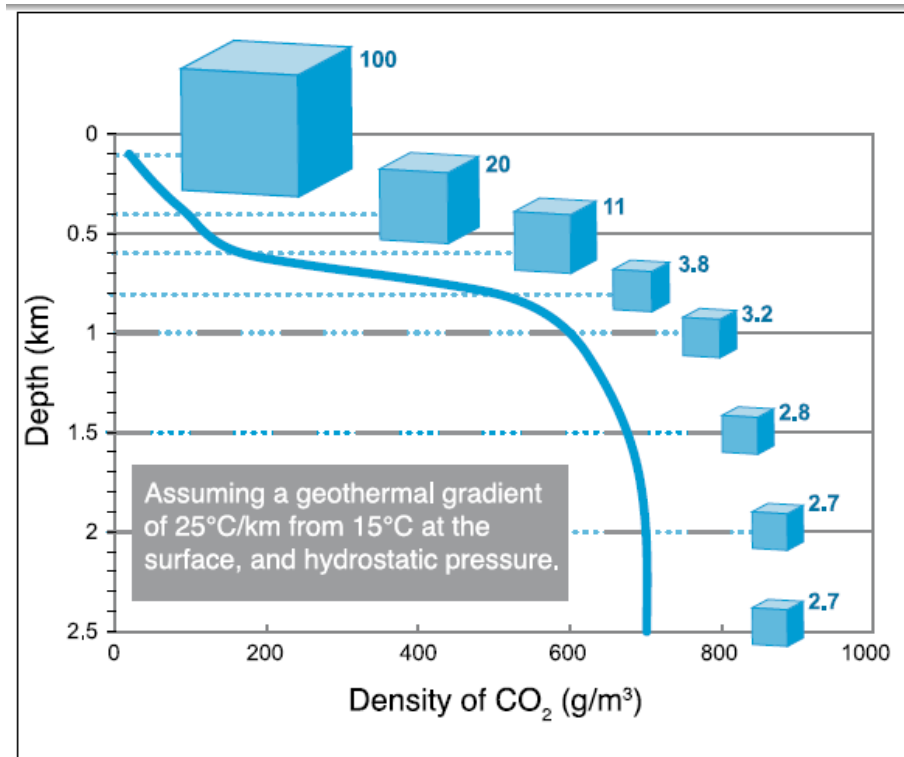


Figure 2.4 Variation of CO₂ density with depth. The change in cube size represents a change in relative volume occupied by the CO₂, not absolute change (from IPCC, 2005).

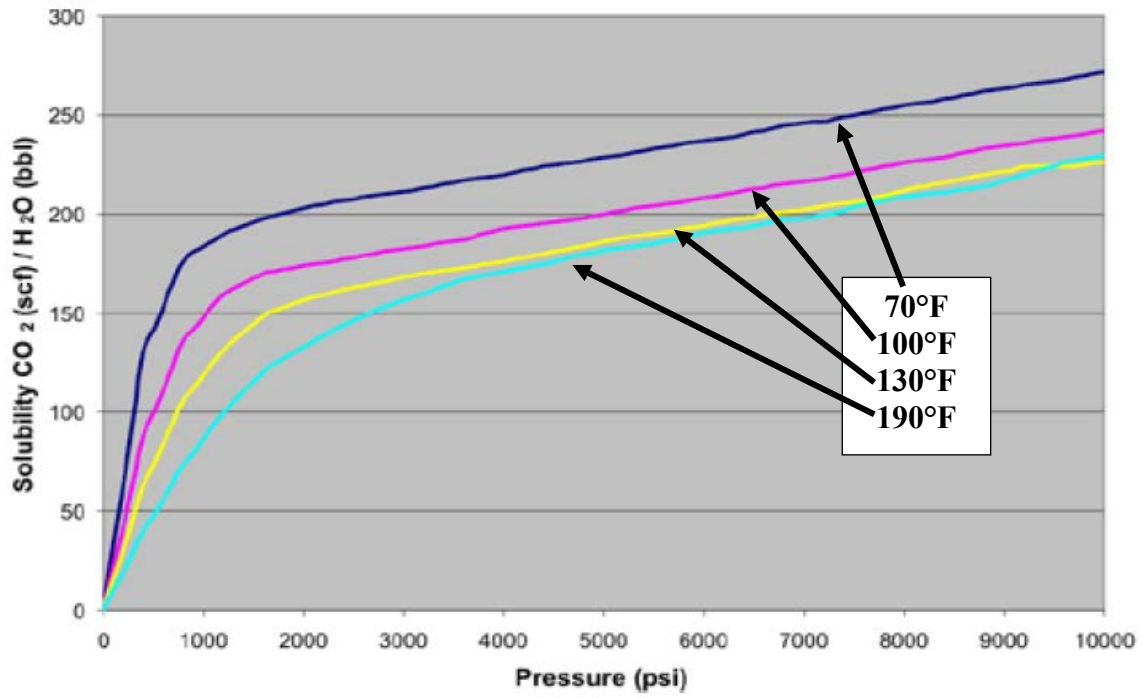


Figure 2.5 CO₂ solubility at different temperatures and pressures (from Carr *et al.*, 2003; Greb and Harris, 2009).

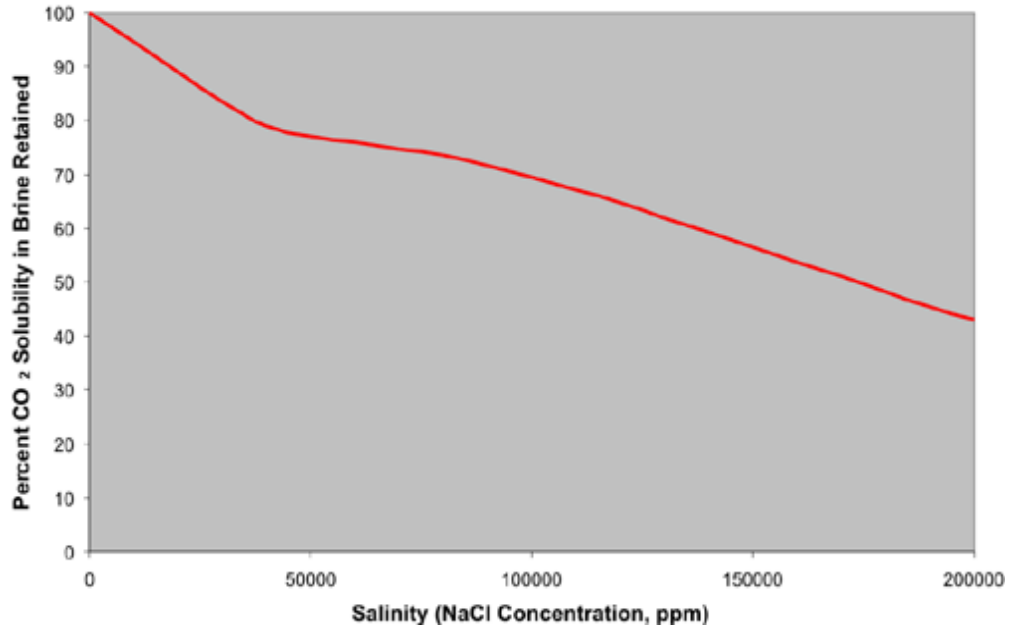


Figure 2.6 Decreasing percent CO₂ solubility versus increasing salinity, which typically increases with depth (from Carr *et al.*, 2003).

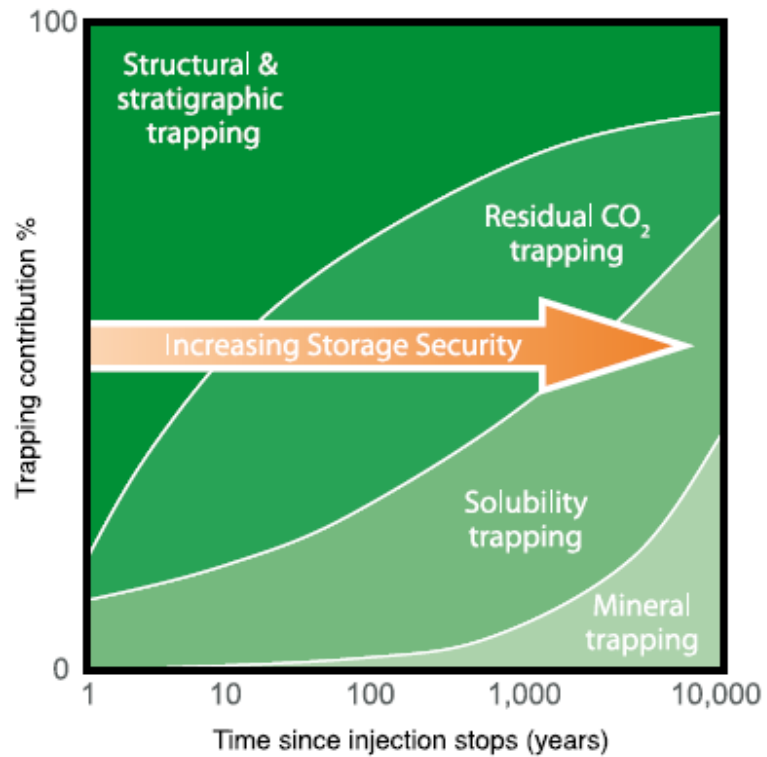


Figure 2.7 CO₂ storage security in the reservoir depends on a combination of both physical and geochemical trapping mechanisms. As time increases, solubility and mineral trapping increase (from IPCC, 2005).



Figure 2.8 Location of the Sugar Creek oil reservoir in Hopkins County, Kentucky (courtesy of R. Locke, ISGS).

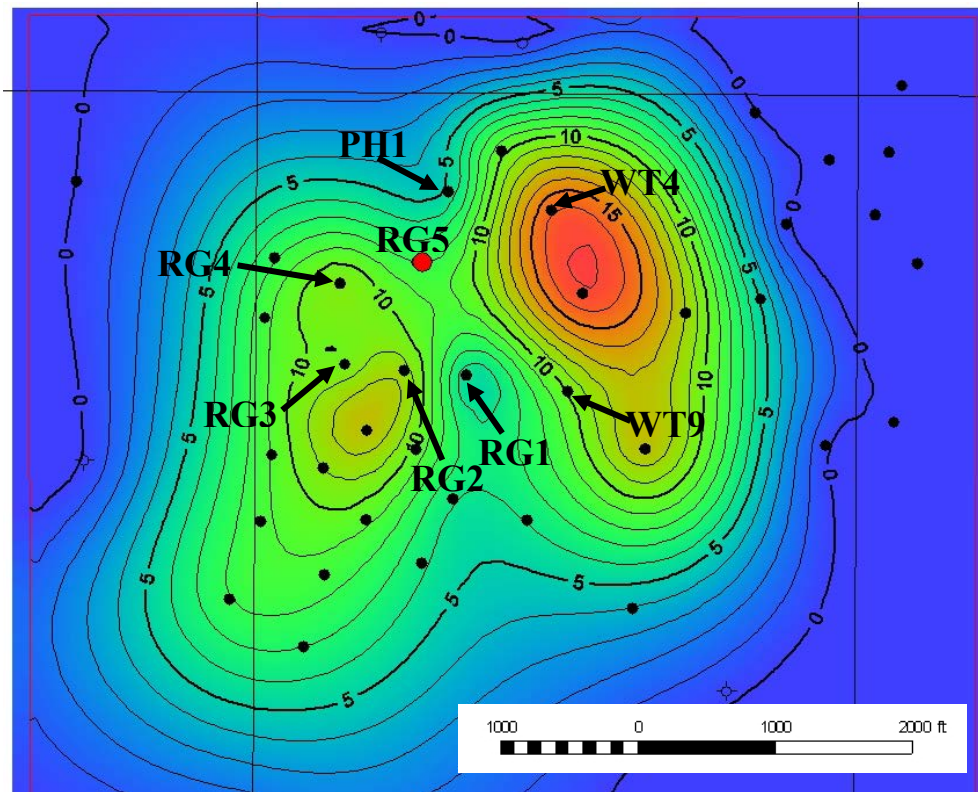


Figure 2.9 Isopach map at Sugar Creek showing thickness of the Jackson in feet. Wells from which formation water and other samples were collected are labeled with abbreviated names (see text). Production wells are shown as black dots and the injection well is a red dot. The WT3 well is not shown on the map (Courtesy of J. Damico *et al.*, ISGS).

Chapter 3: Methods

Accurate characterization of reservoir fluid chemistry and reservoir mineralogy was needed in order to obtain the correct inputs for simulating potential CO₂-water-rock interactions. A total of 62 newly acquired formation fluid samples and measurements from Sugar Creek along with archived water data (collected by KGS and USGS) were used to characterize formation water chemistry. The mineralogy of the reservoir and cap rocks was determined by X-ray diffraction (XRD) measurements on rock core and cuttings samples taken near or in the study field. The collective water chemistry and mineralogical data were then analyzed and input into the GWB for modeling equilibrium state and potential subsurface interactions.

3.1 Formation Water Collection and Laboratory Analysis

Formation waters typically coexist with oil and gas to produce a multi-phase fluid state in hydrocarbon-bearing reservoirs. The Sugar Creek formation water was sampled from the oil reservoir for analysis of various parameters. Each sample was identified by the well name, and a record number was assigned from the KGS oil and gas online database (Table 3.1).

The sampling procedures were adopted and modified from those developed by the Illinois State Geological Survey (ISGS, 1993). The sampled wells were constructed so that all stratigraphic intervals above the oil reservoir were isolated from the wellbore by cement and steel casing. The casing either extended to the top of the reservoir, leaving it exposed to the wellbore (also known as open-hole), or it extended across the reservoir. In the latter example, the casing was perforated to allow fluids to circulate from the

reservoir into the wellbore. Even in the open-hole example, the reservoir interval was typically perforated to facilitate fluid flow into the wellbore. Both examples provided the opportunity to collect discrete samples from the oil reservoir without contamination by mixing with waters from other reservoirs penetrated by the well. Formation water samples were collected using a closed sampling system in which fluids had minimal contact with the atmosphere. This reduced degassing problems and atmospheric contamination. The sampling system consisted of a separation carboy for density segregation of the oil and water, a pre-filter for removing additional oil from the water, and a flow-through cell containing a YSI multi-meter (model 556 MPS) for measuring water properties. These properties included pH, Eh, specific conductance, temperature, and dissolved oxygen (DO). The sampling apparatus was connected to the well head and elements in the sampling system were interconnected with ¼-inch Tygon™ tubing (Figure 3.1). Samples were collected at the point in which water properties, as measured with the YSI multi-meter, became constant and dissolved oxygen levels were less than 1.0 mg/L, which indicated that samples were representative of the formation water.

Samples were then collected for measurement of total CO₂, alkalinity, dissolved inorganic carbon (DIC), anions, metals and cations, and total dissolved solids (TDS) in the KGS lab. Samples were collected in pre-washed Nalgene™ bottles, and all samples, except total CO₂, were filtered with a 0.45 micron filter. Metal and cation samples were acidified with nitric acid to a pH value of 2. After collection, all samples were chilled for transport. Total CO₂ was analyzed according to the American Society for Testing and Materials (ASTM) using a gas-sensing electrode test method (ASTM D 513, 1988). Alkalinity and DIC were analyzed using electrometric titration and a CO₂ coulometer,

respectively (ASTM, 1992; UIC, 2010). A well-mixed sample was dried to 180°C to measure total dissolved solids (ASTM, 1997). Anions and cations in the formation water were analyzed using ion chromatography (ASTM, 1988). Sample collection and measurement quality were monitored using charge balance and only samples with charge balances equal to or less than 10% were used (Table 3.2). Charge balances were calculated using the AquaChem v5.1 software (Schlumberger Water Services, 2010).

3.2 Archived Water Data

Archived hydrochemical data collected in the late 1960's and early 1970's, mostly from oil wells and a few waste disposal and water wells, constituted a supplemental data set. Chemical measurements included major cation and anion concentrations (mg/L), and water property measurements including pH, conductivity, density, and TDS. In addition to the chemical data, the archived records included critical administrative information about the well and its location, and the depth and stratigraphic interval sampled (Parris *et al.*, 2010). For this study, four records from the Jackson Sandstone reservoir in or near the Sugar Creek field were selected to provide representative compositions of Mississippian formation water. Only samples that predated water flood operations were used in order to avoid possible mixing of formation water from different reservoirs. As with the new measurements, only samples with charge balances equal to or less than 10% were used (Table 3.3).

3.3 Mineralogical Analysis

X-ray diffraction (XRD) measurements for mineralogical composition were performed on 17 samples collected from well cuttings near or within the study field. Because of limited amounts of available Jackson cuttings, thin-sections were unable to be produced. When available, geophysical electric logs were used to identify porous and permeable intervals to sample in the reservoir. Of the 17 samples collected, three were from the shaley mudstone upper unit of the Jackson and are referenced henceforth as the seal rocks in Sugar Creek. With lower porosity than the rest of the Jackson, the seal rocks serve as the principal barrier to CO₂ migration.

Mineralogical composition was measured with XRD on the whole-rock and clay fraction (less than 5 microns) by K/T GeoServices. After samples were cleaned of contaminants, XRD measurements were performed using a Rigaku automated diffractometer equipped with a copper X-ray source and a scintillation X-ray detector. Determination of mineral amounts was done by using integrated peak areas and empirical reference intensity ratio factors. The weight percentage data from this method are semi-quantitative and can quantify crystalline material only. The percentages reported for each mineral depend on the percentages for the other materials. One limitation of this method is that if one mineral is underestimated, then the others will be overestimated. Additionally, detection limits differ for each mineral species and are on the order of one to five weight percent (K/T GeoServices, 2008).

3.4 Other Measurements

Though not an explicit part of this study, two additional types of measurements were conducted at Sugar Creek that provide insight into the fate of injected CO₂ and water-rock interactions. The first were stable isotope measurements ($\delta^{18}\text{O-H}_2\text{O}$, $\delta\text{D-H}_2\text{O}$, $\delta^{13}\text{C-DIC}$) of the formation waters. These samples were collected at the same time samples were collected for the bulk chemistry measurements. The second were bulk and isotopic composition measurements ($\delta^{13}\text{C-CO}_2$, $\delta^{13}\text{C-CH}_4$) of gases co-produced with oil and the formation waters, which was important for calculating gas fugacities and determining the timing of CO₂ break-through. Bulk gas composition was measured in the field with an infrared gas analyzer on gas produced up the wellbore annulus. Gas samples collected from the annulus were used to measure bulk and stable isotopic composition at the Illinois State Geological Survey and Isotech Laboratories.

3.5 Modeling: Geochemist's Workbench Software

Geochemist's Workbench (GWBTM) version 8.0 was used for equilibrium, reaction-path, and kinetic modeling of CO₂-water-rock interactions. GWB is a commercial geochemical reaction and transport modeling package that consists of a suite of modules that solve different types of geochemical problems, and manage and analyze a variety of geochemical data. In order of increasing complexity the modules include SpecE8, React, and X1t and X2t. The SpecE8 module is a speciation or "closed system" model in which mass is not exchanged between the system of interest and its surrounding environment. Measured or inferred fluid chemistry values are used as inputs to predict the

distribution of components among aqueous species. Mineral saturation states are also predicted along with the reaction directions needed to attain equilibrium.

The React module is an “open system” model in which the system exchanges mass or energy with its surrounding environment. Reaction-path models use the speciation calculation as a starting point, but then follow this with a series of speciation calculations to document changes in the composition of the system due to changes in temperature, Eh, pH, gas fugacities, species concentrations, mineral mass, or some combination thereof. This allows for the forward predictions of changes in fluid chemistry and mineral composition and mass along the reaction path.

The X1t (1-dimensional) and X2t (2-dimensional) modules are reactive transport models in which a series of reaction-path models are represented by points distributed over a certain spatial domain. Mass transport in the reaction-path models allows the user to describe the movement of fluid and the transport of chemical species due to advection, dispersion and diffusion. Although no reactive transport modules were used for this study, modeling reactions under no-flow conditions is still an important tool in analyzing and predicting geochemical reactions and the variables that control reaction progress and products (Bethke, 2008).

3.5.1 Conceptual Model and Strategies

To develop an effective geochemical model, the system or process of interest must be conceptualized in a useful manner with the heart of the model being the equilibrium system. In this study the equilibrium system is assumed to be closed at a constant temperature (i.e. isothermal), and contains formation fluids and gases, and reservoir minerals. These components act as the basis species for constructing a

representative geochemical model and provide a starting point for the reaction-path models (open systems) to trace changes in the system's equilibrium state (Bethke, 2008).

As a starting point, it was necessary to define the equilibrium system in the reservoir prior to any chemical changes related to the injection of CO₂. Under isothermal conditions, bulk water chemistry values, gas fugacities, and mineral masses were input into the SpecE8 and React modules to define the equilibrium system. Collectively, these inputs constituted the basis species for the geochemical model. SpecE8 and React used the basis species to describe the composition of all phases and species, charged and uncharged, in the system (Zhu and Anderson, 2002). Once the reservoir or basis was sufficiently characterized, it was used in the React module for reaction-path modeling to trace changes in aqueous species concentrations and the precipitation and dissolution of minerals as CO₂ was introduced into the system.

Because fluid transport was not incorporated into this study, it was not possible to explicitly simulate spatial variations in water-rock interactions due to variation in CO₂ concentration. From a geochemical process perspective, though, variations in CO₂ concentration and their effect on reactions were examined within the context of varying CO₂ fugacity (henceforth called $f\text{CO}_2$). The geochemical system of interest for this study is the reservoir and overlying seal rocks, where $f\text{CO}_2$ varies from a maximum value at and near the injection well to a pre-injection $f\text{CO}_2$ at some distance from the injection well. The $f\text{CO}_2$ was determined by first calculating variations in CO₂ partial pressure at the production and injection wells. The partial pressure of CO₂ equaled the product of reservoir pressure (measured or estimated) and the concentration of CO₂ measured with an infrared gas analyzer in the annular space gas. The $f\text{CO}_2$ equaled the product of CO₂

partial pressure (P_{CO_2}) and the fugacity coefficient (ϕ). Fugacity coefficients for reservoir conditions were calculated using an online calculator (Duan *et al.*, 1992).

Under conditions of active injection it was assumed that gas at and near the injection wells consisted primarily of CO_2 and therefore CO_2 partial pressure equaled total pressure. Table 3.4 shows the pressures and fugacities at Sugar Creek. The bottom-hole injection pressure (1900 psi, 129.2 bars) was continuously recorded with a bottom-hole pressure transducer (Frailey, *et al.*, 2012). Bottom-hole pressures in the Sugar Creek production wells were estimated to be significantly less (30 psi, 2.04 bars) because of field operating procedures (M. Gallagher [field operator], personal communication).

In addition to the calculated fugacities at the injection and production wells, a median f_{CO_2} and between the injection and production wells was selected to represent geochemical reactions under conditions of intermediate CO_2 concentration (Table 3.4). It should be emphasized, however, that the median fugacity, henceforth called the mid-fugacity, simulation need not correspond with a geographic point midway between the injection well and any given production well. Moreover, gas and water chemistry measurements at Sugar Creek show that the decrease in CO_2 away from the injection well did not occur in a regular radial pattern.

The infrared gas measurements showed that the majority of associated gas in the reservoir prior to CO_2 injection consisted of CH_4 . It was assumed that the aqueous reservoir fluid was saturated with respect to CH_4 because it was in contact with hydrocarbons. The saturation value for CH_4 was included in the basis as a fugacity calculation. The composition of CH_4 in the formation water was determined from an online calculator for reservoir temperature (28°C), and the previously mentioned

pressures in 1 m NaCl formation water (Duan and Mao, 2006). Small amounts of CO₂ were also detected in some wells and it too was included in the basis as a fugacity calculation (Table 3.4).

The final step in representing geochemical conditions in the reservoir prior to CO₂ injection was simulated using the React module by adding the reservoir minerals as simple reactants with the formation water containing background levels of CO₂ and CH₄. The resulting equilibrium model provided a starting point for documenting subsequent changes in water properties (e.g. pH, alkalinity) and mineral saturation states due to CO₂ injection.

A sliding $f\text{CO}_2$ model was used to simulate the effects of CO₂ injection on the pre-CO₂ speciated formation water. The $f\text{CO}_2$ was raised to maximum injection pressure with no minerals in the system. The results from this simulation were “picked up” and reservoir minerals were titrated in for 365 days to represent the year of CO₂ injection. Although the order of operations is not completely intuitive relative to how CO₂ injection occurs in real life, to run GWB required CO₂ to be injected into the formation water and then the minerals to be titrated in as separate steps. The post-injection phase of the geochemical model was simulated by sliding $f\text{CO}_2$ back down to a pre-injection value with reservoir minerals treated again as simple reactants.

3.5.2 Model Inputs and Calculations

Several preliminary calculations, such as mineral mass and surface area, were needed to characterize reservoir conditions and quantify model inputs. First, GWB requires the user to define the masses of water and rock in the reaction simulations. This defines the water:rock ratio, which exerts a strong influence on the extent and magnitude

of reactions. The default simulation mass is 1 kg of water, and average porosity and water saturation data (Table 3.5) were used to calculate the reservoir mass and volume needed to hold 1 kg of water. Total reservoir volume ($V_{\text{reservoir}}$) is the sum of the rock volume (V_{rock}), oil-saturated volume (V_{oil}), and water-saturated volume (V_{water}). As demonstrated in Figure 3.2a, if total reservoir volume equals “x” then rock, oil, and water volumes represent some fractional “x”. Assuming a water density of 1050kg/m^3 , the volume occupied by 1 kg of water equals the mass divided by density. Therefore, the volume of reservoir, x, needed to hold $9.5 \times 10^{-4} \text{ m}^3$ of water equals V_{water} (water-saturated pore volume of the reservoir). Previous calculations by the field operator showed oil and water saturation to equal 65% and 35%, respectively (M. Gallagher [field operator], personal communication). Sugar Creek does not have an underlying aquifer and therefore a single water-filled porosity value was applied to the whole Jackson Sandstone reservoir.

Once the reservoir volume was calculated, the rock volume was calculated as the product of the reservoir volume and the fractional rock volume- in this case, 84%. Rock volume was converted to rock mass assuming a density of $2,650 \text{ kg/m}^3$. This density was used since the reservoir is quartz-rich sandstone. The mass of any given mineral in the reservoir equaled the product of total rock mass and relative weight percent of that mineral as determined from the XRD analysis (Figure 3.2b). The same equations were used to calculate volumes and masses in the seal rocks, but a lower porosity (3%) was used and it was assumed to be 100% water saturated. Lower porosity in the seal rocks produced water-rock ratios that were approximately 50% less than that in the reservoir rocks (Table 3.5).

Kinetic simulations in the React module required surface areas and rate constants for minerals in the reservoir and seal rocks (Table 3.6). Rate constants were compiled from a variety of sources (White and Brantley, 1995; Gunter *et al.*, 1997; Pokrovsky and Schott, 2001; Arvidson *et al.*, 2003; Palandri and Kharaka, 2004; Brantley, 2008; Bandstra *et al.*, 2008). Figure 3.3 is an example of the surface area calculation for quartz in the Jackson using the XRD mineral mass determined in Figure 3.2b. To estimate surface area, it was assumed that mineral grains were spherical with a diameter of 0.1875 mm. This grain size diameter equals the median value for fine-grained sand (Wentworth, 1922), which was chosen because the Jackson reservoir consists largely of well-sorted, fine-grained sandstone with well-rounded quartz grains. The density of quartz was multiplied by the sphere volume to get the quartz mass per sphere. The previously calculated total mineral mass (Figure 3.2b) was divided by the mass per sphere to give the number of quartz spheres. Then, the total number of spheres was multiplied by the surface area of a sphere to give an estimated maximum total surface area for quartz in the simulation volume. Similar calculations were applied to other minerals in the reservoir and seal rocks (Table 3.6). It should be noted that this estimate of reactive surface area represents a maximum value as it is assumed that the entire mineral surface area is exposed to fluid and therefore available for reactions. In reality, this is not the case because where the grains contact each other those surfaces are not in contact with fluid.

Table 3.1 Administrative information for wells from which water data were collected and/or analyzed. Record number refers to the KGS database identification number corresponding to each well. Dashes mean that no data were available.

Record No.	Well Name	Field Name	County	Elevation (ft)	Sampled Interval	Remark	Source
53776	Pressley-Hart #1 (PH1)	Sugar Creek	Hopkins	488	Jackson	Production well	This study
53419	Ross Gentry #1 (RG1)	Sugar Creek	Hopkins	497	Jackson	Production well	This study
53418	Ross Gentry #2 (RG2)	Sugar Creek	Hopkins	512	Jackson	Production well	This study
53417	Ross Gentry #3 (RG3)	Sugar Creek	Hopkins	497	Jackson	Production well	This study
53416	Ross Gentry #4 (RG4)	Sugar Creek	Hopkins	510	Jackson	Production well	This study
53415	Ross Gentry #5 (RG5)	Sugar Creek	Hopkins	497	Jackson	Injection well	This study
54162	Wilbur Todd #3 (WT3)	Sugar Creek	Hopkins	430	Jackson	Water injection well	This study
54163	Wilbur Todd #4 (WT4)	Sugar Creek	Hopkins	507	Jackson	Production well	This study
131562	Wilbur Todd #9 (WT9)	Sugar Creek	Hopkins	494	Jackson	Production well	This study
53419	Ross Gentry #1	Sugar Creek	Hopkins	493	Jackson	5/11/70	Archived
10960	Clements #1	-	Hopkins	476	Jackson	-	Archived
2025940	Hoover Hrs. #1	Huntsville CONS	McLean	390	Jackson	8/15/72	Archived
2030172	Delmore Collier #1	Elba West CONS	Muhlenburg	482	Jackson	5/19/1968	Archived

Table 3.2 Charge balance analysis (% electroneutrality) for Jackson formation waters collected in this study. WT3 samples are from a Pennsylvanian sandstone aquifer, which supplied some injection water in the field. Well abbreviations are defined in Table 3.1.

Well Abbrev.	Sample Round	Sample Date	% Electroneutrality
RG1	1	3/16/2009	-3.81
RG1	2	4/8/2009	-6.4
RG1	9	11/9/2009	-0.13
RG1	10	12/10/2009	-2.43
RG1	13	3/2/2010	-1.95
RG2	2	4/8/2009	-4.56
RG2	3	4/28/2009	-0.61
RG2	4	6/2/2009	-4.77
RG3	1	3/17/2009	-5.35
RG3	3	4/28/2009	-1.02
RG3	4	6/2/2009	-1.78
RG3	5	6/29/2009	-4.01
RG3	6	8/10/2009	-0.78
RG3	7	9/8/2009	-2.02
RG3	8	10/12/2009	-1.13
RG3	9	11/10/2009	-0.24
RG3	10	12/10/2009	-0.89
RG3	11	1/13/2010	0.1
RG3	12	2/2/2010	3.04
RG3	13	3/2/2010	-0.98
RG4	1	3/17/2009	-2.22
RG4	2	4/7/2009	0.8
RG4	3	4/27/2009	-0.75
RG4	4	6/2/2009	-0.1
RG4	5	6/29/2009	-2.06
RG4	6	8/10/2009	-3.19
RG4	7	9/8/2009	-2.07
RG4	8	10/12/2009	0.89
RG4	9	11/10/2009	-1.37
RG4	10	12/10/2009	0.49
RG4	11	1/13/2009	0.33
RG4	12	2/2/2010	1.39
RG4	13	3/2/2010	-1.63
RG5	1	3/16/2009	-3.39

Table 3.2 (continued) Charge balance analysis (% electroneutrality) for Jackson formation waters collected in this study. WT3 samples are from a Pennsylvanian sandstone aquifer, which supplied some injection water in the field. Well abbreviations are defined in Table 3.1.

Well Abbrev.	Sample Round	Sample Date	% Electroneutrality
PH1	2	4/8/2009	-5.91
PH1	3	4/28/2009	-1.65
PH1	4	6/3/2009	-6.55
PH1	5	6/29/2009	-4.38
PH1	6	8/10/2009	-4.01
PH1	8	10/13/2009	0.08
WT3	6	8/11/2009	-12.32
WT3	9	11/10/2009	-6.58
WT3	12	2/2/2010	-2.45
WT4	3	4/28/2009	-1.33
WT4	4	6/3/2009	-4.39
WT4	5	6/29/2009	-5.73
WT4	6	8/11/2009	-5.97
WT4	7	9/9/2009	-0.12
WT4	8	10/13/2009	-0.08
WT4	9	11/9/2009	-1.15
WT4	11	1/13/2010	-0.45
WT4	12	2/2/2010	3.42
WT4	13	3/2/2010	-3.2
WT9	3	4/29/2009	-1.2
WT9	4	6/3/2009	21.41
WT9	5	6/29/2009	-0.65
WT9	6	8/11/2009	-12.32
WT9	7	9/9/2009	-3.81
WT9	8	10/13/2009	0.9
WT9	9	11/10/2009	-0.09
WT9	9a	11/18/2009	5.94
WT9	10	12/10/2009	-0.12
WT9	11	1/13/2010	-0.72
WT9	12	2/2/2010	1.91
WT9	13	3/2/2010	1.79

Table 3.3 Charge balance analysis (% electroneutrality) for archived water samples from the Jackson collected near Sugar Creek.

Brine_No.	County	Sampled Interval	% Electroneutrality
Hop29	Hopkins	Jackson	0.00
Hop152	Hopkins	Jackson	-1.26
McL2	McLean	Jackson	-1.24
Muhl4	Muhlenburg	Jackson	-0.28

Table 3.4 Calculated CO₂ fugacity and CH₄ solubility for the pre-injection and CO₂-injection simulations. The CO₂ fugacity coefficient (Duan *et al.*, 1992) and CH₄ solubility (Duan and Mao, 2006) were determined with an online calculator using input values of reservoir temperature, pressure, and molar concentration of NaCl in the formation water.

		Sugar Creek			
		Injection Well (RG5)	Mid- Fugacity	Avg. Production Wells (RG1-4, WT9)	Avg. Production Wells (WT4/PH1)
Pre-Injection	Total pressure (psi/bar)	700/47.6		30/2.04	
	CO ₂ concentration	3.5%			
	CO ₂ co-efficient	0.7737		0.9899	
	CO ₂ partial pressure (psi/bar)	24.5/1.67		1.05/0.0714	
	CO ₂ fugacity (bar)	1.29		0.0707	
	CH ₄ solubility (mol/kg)	0.05045		0.00241	0.00208
Injection	Total pressure (psi/bar)	1900/129.2	-	30/2.04	
	CO ₂ concentration	100%	-	83%	
	CO ₂ co-efficient	0.5921	-	0.9917	
	CO ₂ partial pressure (psi/bar)	1200/81.6	-	24.9/1.69	
	CO ₂ fugacity	49.6	25.6	1.68	

Table 3.5 Porosity and phase saturation data for reservoir and seal rocks. Total porosity represents an average based on core analysis of the Jackson in the area of Sugar Creek. Oil- and water-filled porosity values are based on phase saturation calculations by the field operator that yielded oil and water saturations equal to 65% and 35%, respectively (M. Gallagher [field operator], personal communication). Note: Values represent conditions at the onset of field development and before the water flood operation.

Sugar Creek	
Reservoir Total Porosity (ϕ_{total})	16%
Oil Porosity (ϕ_{oil})	10.4%
Water Porosity (ϕ_{water})	5.6%
Seal Rock Total Porosity (ϕ_{total})	3%
Water Porosity (ϕ_{water})	3%
Water:Rock (reservoir)	0.07
Water:Rock (seal)	0.03

Table 3.6 Inputs for kinetic simulations included surface areas calculated in this study and rate constants compiled from the literature. Dolomite and Chlinochlore-14A were used as substitutes for ankerite and chlorite, respectively, due to lack on thermodynamic data available within the GWB software (¹Brantley, 2008; ²Arvidson *et al.*, 2003; ³Pokrovsky and Schott, 2001; ⁴Gunter *et al.*, 1997; ⁵Rockware, Inc. GWB Short-course, unpublished, 2009; ⁶Palandri and Kharaka, 2004; ⁷White and Brantley, 1995).

Mineral	Surface Area (cm²/grams)	Rate Constant (mol/cm² sec)
¹ Quartz	120.75	7×10^{-17}
¹ K-feldspar	125.00	6×10^{-17}
¹ Albite	122.14	9×10^{-17}
² Calcite	118.08	1×10^{-10}
³ Ankerite (Dolomite)	112.68	1×10^{-12}
⁴ Siderite	80.81	1×10^{-10}
⁵ Pyrite	63.87	3.05×10^{-17}
⁶ Gypsum	139.13	1.62×10^{-7}
⁷ Illite	116.36	1×10^{-13}
⁵ Smectite	116.36	2.3×10^{-22}
¹ Kaolinite	123.08	8×10^{-19}
⁷ Chlorite (Chlinochlore-14A)	100.00	1×10^{-13}
⁵ Hematite	60.38	3.05×10^{-17}



Figure 3.1 Photo showing the field setup apparatus used to sample formation waters. Oil was separated from formation water in the separation carboy. The outflow water from the separation carboy was further filtered before entering the flow-through cell for the YSI multi-meter. The large waste carboy on the ground collects overflow (photo by G. Beck, 2009).

(a)

$$V_{\text{rock}} + V_{\text{oil}} + V_{\text{water}} = V_{\text{reservoir}}$$

$$0.84x + 0.104x + 0.056x = x$$

Where:

$$V_{\text{reservoir}} = x$$

$$V_{\text{rock}} = (1 - \phi_{\text{total}})x = 0.84x$$

$$V_{\text{oil}} = 0.104x$$

$$V_{\text{water}} = 0.056x$$

$$\phi_{\text{total}} = 16\%$$

$$\phi_{\text{oil}} = 10.4\%$$

$$\phi_{\text{water}} = 5.6\%$$

$$\rho_{\text{water}} = 1054.7 \text{ kg/m}^3 \text{ (measured density of formation waters in field)}$$

$$\rho_{\text{rock}} = 2650 \text{ kg/m}^3 \text{ (density of quartz)}$$

$$V_{\text{water}} = 1 \text{ kg} / (1054.7 \text{ kg/m}^3) = 9.48 \times 10^{-4} \text{ m}^3$$

$$9.48 \times 10^{-4} \text{ m}^3 = V_{\text{water}} = 0.056x;$$

$$\text{So reservoir volume, } x = 1.69 \times 10^{-2} \text{ m}^3$$

$$V_{\text{rock}} = 0.84 (1.69 \times 10^{-2} \text{ m}^3) = 1.42 \times 10^{-2} \text{ m}^3$$

$$M_{\text{rock}} = (1.42 \times 10^{-2} \text{ m}^3)(2650 \text{ kg/m}^3) = 37.7 \text{ kg}$$

(b)

To find mineral masses, take M_{rock} and multiply by XRD weight percent results for each mineral:

$$M_{\text{mineral}} = (\text{weight percent})(M_{\text{rock}})$$

Where:

$$\text{Quartz} = 80.4\%$$

$$M_{\text{quartz}} = 0.804 (37.7 \text{ kg}) = 30.3 \text{ kg}$$

Figure 3.2 Sample calculations explaining how (a) water-saturated and rock volumes and masses in the reservoir were calculated, and (b) how mineral masses were estimated. The example in (b) is for quartz in the Jackson.

$$V_{\text{mineral}} = (4/3)(\Pi)(r^3)$$

Where:

V_{mineral} = volume of mineral sphere

r = radius of mineral sphere

$$V_{\text{quartz}} = (4/3) (\Pi) (r^3)$$

$$V_{\text{quartz}} = (4/3) (\Pi) ((0.009375\text{cm})^3)$$

$$V_{\text{quartz}} = 3.45 \times 10^{-6} \text{ cm}^3$$

Where:

$$r = (0.1875 \text{ mm} / 2) = (0.01875 \text{ cm} / 2) = 0.009375 \text{ cm}$$

$$M_{\text{qtz grain}} = (\rho_{\text{quartz}}) (V_{\text{quartz}})$$

$$M_{\text{qtz grain}} = (2.65 \text{ g/cm}^3) (3.45 \times 10^{-6} \text{ cm}^3)$$

$$M_{\text{qtz grain}} = 9.146 \times 10^{-6} \text{ g}$$

Where:

$$\rho_{\text{quartz}} = 2.65 \text{ g/cm}^3$$

$$\text{Number of grains} = M_{\text{total}} / M_{\text{qtz grain}}$$

$$\text{Number of grains} = 30,303 \text{ g} / 9.146 \times 10^{-6} \text{ g}$$

$$\text{Number of grains} = 3.313 \times 10^9$$

Where:

$$M_{\text{total}} = 30.303 \text{ kg} = 30,303 \text{ g} \text{ (from Figure 3.2b)}$$

$$\text{Surface Area}_{\text{total}} = (4(\Pi)(r^2)) (\text{Number of grains})$$

Where:

Surface Area = surface area per sphere

r = radius of mineral sphere

$$\text{Surface Area}_{\text{total}} = (4(\Pi)((0.009375 \text{ cm})^2) (3.313 \times 10^9)$$

$$\text{Surface Area}_{\text{total}} = 3.659 \times 10^6 \text{ cm}^2$$

$$\text{Surface Area} = \text{Surface Area}_{\text{total}} / M_{\text{total}}$$

$$\text{Surface Area} = 3.659 \times 10^6 \text{ cm}^2 / 30,303 \text{ g}$$

$$\text{Surface Area} = 120.75 \text{ cm}^2/\text{g}$$

Figure 3.3 Calculations of mineral surface area using quartz as an example.

Chapter 4: Water Chemistry and Mineralogy Results and Discussion

4.1 Formation Water Chemistry

The chemistry of formation waters at Sugar Creek is based on 62 samples collected at eight wells from May 2009 through May 2010. The majority of the samples were collected during injection (ten sample rounds) with a smaller number collected before (three sample rounds). Table 4.1 shows the average values of all the rounds for each well. In addition, four archived samples were used to complement the new samples. The archived water chemistry data are important because they are interpreted to represent pristine Mississippian formation waters and, as such, provide a useful reference in determining to what degree water flooding at Sugar Creek has altered the chemistry of formation waters. Piper plot analysis of formation waters at Sugar Creek shows that they consist primarily of Na^+ and Cl^- (Figure 4.1). The Piper plots also show little difference in the relative proportion of the major cations and anions before and during CO_2 injection (Figure 4.2). The exception is WT3 because it is significantly more enriched in HCO_3^- and has lower TDS values of 664 to 936 mg/L.

While the Piper plots are effective in showing variation in the relative proportion of major cations and anions, they do not show changes in absolute concentrations where proportions are relatively constant. This is demonstrated in a plot of $\text{Na}+\text{Cl}$ versus total dissolved solids (Figure 4.3). Sugar Creek formation waters group into two distinct populations, with the PH1 and WT4 wells having TDS values ranging from 50,420 to 66,640 mg/L, whereas the RG1-RG5 and WT9 wells have significantly lower TDS values on the order of 11,124 to 28,740 mg/L. The WT3 well, with even lower TDS values (664 to 936 mg/L) plots in the upper left corner of Figure 4.3. The variation in water chemistry

shown in Figure 4.3 likely results from varying degrees of mixing between the more dilute Pennsylvanian water from WT3 with more saline Jackson formation water. The differences suggest that Jackson formation water in PH1 and WT4 was minimally impacted, if at all, by water flooding. Therefore, salinity in PH1 and WT4 might represent native formation water salinity. In contrast, salinity was reduced by approximately 50% in WT9 and RG1-RG5 by mixing with less saline Pennsylvanian water from WT3. The bimodal distribution of TDS values provides evidence that the Jackson reservoir is compartmentalized with RG1-RG5 and WT9 being in hydrologic communication with each other, whereas PH1 and WT4 appear to be isolated by some unknown geologic barrier. Despite the differences in salinity and Na+Cl concentration, both the high and low salinity populations show a slight excess of TDS compared to the Na+Cl concentration, indicating the contribution of other cations (Ca^{2+} , Mg^{2+}) and anions (SO_4^{2-} , HCO_3^-) to TDS.

Of the archived data from the Jackson, four out of ten samples collected between 1966 and 1970 have charge balances of 10% or less and were in Hopkins or an adjacent county. Initial Piper plot analysis shows the archived waters to contain primarily Na^+ and Cl^- , which is consistent with results from the newer samples collected from Sugar Creek (Figure 4.4). Plotting Na+Cl versus TDS for the archived samples shows a range of TDS values to be 17,600 to 59,200 mg/L (Figure 4.3). By analogy, the range in TDS and Na+Cl suggests that some of the archived Jackson formation water samples might have also been diluted in the water flood operations in surrounding fields.

4.2 Mineralogy and Petrography

XRD analyses of reservoir and seal rocks in the Jackson allowed identification of potentially reactive minerals and provided semi-quantitative estimates of mineral masses used as inputs for GWB. Macroscopic examination of 14 Jackson reservoir samples shows them to be primarily tan to gray, fine-grained sandstone. Three samples from the upper unit of the Jackson (1730, 1780, and 1810 feet) are medium gray, shaley mudstones. Due to limited Jackson cuttings samples, there was not enough material to send out requests for both XRD analysis and thin section preparation.

In accordance with the macroscopic analysis, the XRD results (Table 4.2) show that samples collected from the Jackson reservoir are predominantly composed of quartz (70.6-89.5%), with lesser amounts of feldspars (1.7-4.4%), carbonates (2.4-19.1%) and clays (3.9-14.8%). Without thin sections the distribution and mode of these minerals is unknown; however, petrographic analysis of Chester sandstone samples elsewhere show that detrital quartz is the main framework grain with smaller amounts of detrital feldspar (Siever, 1953). Additionally, several samples contain large amounts of ankerite and correspond to intervals having high resistivity values. The coincidence suggests that the ankerite might be pore-filling cement because it would reduce the pore space available for pore fluids that have lower resistivity as compared to minerals.

Unlike the reservoir rocks, the three samples from the shaley upper Jackson unit (Table 4.2) contain significantly less quartz (25.7-28.6%), and more clays (44.2-60.2%), feldspars (4.2-5.7%), and carbonates (7.8-21.3%). The more clay-rich section of the Jackson could act as an additional sealing layer above the reservoir.

Table 4.1a Average water properties for Jackson formation water sample. For each well name, the top line of the sample round column represents the samples collected before injection of CO₂ (before May 11, 2009) and the bottom line represents samples collected after CO₂ injection had occurred.

Well Name	No. of Sample Rounds Averaged	pH	Temp (°C)	Cond (mS/cm)	Eh (mV)	DO (mg/L)	Alkalinity (mg/L, CaCO₃)	TDS (mg/L)
PH1	2	7.11	18.2	89.1	-188.6	0.55	186	58101
	4	6.77	22.9	87.2	-135.8	1.74	619	61654
WT4	1	6.84	20.4	83.9	-270.3	0.87	310	50420
	9	6.78	19.8	84.1	-244.5	1.39	328	57474
WT9	1	7.12	18.6	37.8	31.3	2.79	858	23720
	11	6.91	17.0	39.0	-246.3	2.08	943	24317
RG1	2	7.26	17.9	41.8	-229.1	1.04	661	21298
	3	5.70	16.5	43.5	-119.1	1.22	1070	28481
RG2	2	6.67	18.6	48.4	-247.5	2.54	850	25818
	1	6.22	27.7	40.9	-182.9	1.77	1997	27284
RG3	2	6.34	18.8	35.1	-122.1	1.36	882	23554
	10	5.95	20.0	40.0	-192.8	1.11	1505	25945
RG4	3	6.88	20.8	25.5	-255.9	2.67	832	19761
	10	6.16	20.8	34.5	-180.5	1.35	1202	21227
RG5	1	7.16	14.0	25.2	-342.9	0.26	689	19108

Table 4.1b Average water properties for Jackson formation water sample. For each well name, the top line of the sample round column represents the samples collected before injection of CO₂ (before May 11, 2009) and the bottom line represents samples collected after CO₂ injection had occurred. Important cation and anion concentrations are listed in milligrams per liter (mg/L).

Well Name	No. Sample Rounds Averaged	Al ⁺³	Ca ⁺²	Ba ⁺²	Fe ⁺²	Li ⁺	Mg ⁺²	Mn ⁺²	K ⁺	Si ₊₄	Na ⁺	Sr ⁺²
PH1	2	-	1555	3.43	184.25	5.45	600	4.43	51	6.76	16775	321
	4	0.15	1668	2.54	27.50	2.49	621	1.36	46	8.05	16825	343
WT4	1	-	1580	5.61	-	2.42	604	0.39	50	4.27	17340	262
	9	0.10	1563	4.99	-	2.23	593	0.20	47	4.57	16980	279
WT9	1	-	453	1.81	21.00	0.97	183	1.63	25	4.20	7860	528
	11	-	471	2.54	-	1.00	191	0.31	28	6.13	7845	563
RG1	2	-	489	2.10	0.02	3.04	173	0.27	19	5.85	6312	317
	3	-	669	3.04	3.01	1.08	238	0.29	28	6.63	8983	450
RG2	2	-	571	4.80	0.01	2.36	219	0.08	26	5.65	7965	483
	1	-	863	4.47	6.23	0.82	240	1.71	24	7.24	7460	596
RG3	2	-	483	5.21	-	2.14	192	0.12	23	6.29	7240	510
	10	-	659	3.26	3.82	0.93	234	0.87	23	6.80	7872	650
RG4	3	-	385	2.22	0.04	2.06	159	0.15	19	5.98	5895	474
	10	0.08	547	2.32	8.23	0.75	202	0.86	19	5.55	6544	536
RG5	1	-	440	2.89	0.01	2.86	172	0.12	17	5.85	5990	284

Table 4.1c Average water properties for Jackson formation water sample. For each well name, the top line of the sample round column represents the samples collected before injection of CO₂ (before May 11, 2009) and the bottom line represents samples collected after CO₂ injection had occurred. Important cation and anion concentrations are listed in milligrams per liter (mg/L).

Well Name	No. Sample Rounds Averaged	HCO ₃ ⁻	Br ⁻	Cl ⁻	I ⁻	SO ₄ ⁻²
PH1	2	227	128	33150	4.6	8.3
	4	755	145	32950	4.7	14.8
WT4	1	378	125	32100	4.0	54.5
	9	400	132	31833	4.2	104.3
WT9	1	1046	52	13600	1.6	60.1
	11	1149	54	12979	1.9	90.2
RG1	2	805	47	12250	0.9	33.5
	3	1305	63	15800	1.9	49.2
RG2	2	1036	55	14450	1.8	30.9
	1	2435	57	14200	1.5	44.2
RG3	2	1075	50	13200	1.8	27.0
	10	1835	57	13650	1.8	40.1
RG4	3	1014	39	10167	1.5	35.8
	10	1466	47	11340	1.5	63.0
RG5	1	840	41	11000	1.6	34.4

Table 4.2 Summary of XRD mineralogic characterization for the Jackson. Values for each mineral are listed in weight percent.

*Jackson samples collected immediately above the sandstone reservoir have low porosity and permeability and are treated as the seal rocks for the formation. Abbreviations are as follows: Graden Osburn #1-A (GO1A), Gatlin Harris #3 (GH3), Thomason & Boyd #1 (TB1), Wilbur Todd #2 (WT2), and Dexter Laffoon #1 (DL1), quartz (Qtz), potassium feldspar (K-spar), plagioclase (Plag), ankerite (Ank), calcite (Cal), dolomite (Dol), pyrite (Pyr), gypsum (Gyp), kaolinite (Kao), and chlorite (Chlor). Abbreviations for mixed-layer clays are R0 M-L I/S 90S, randomly ordered mixed-layer illite/smectite with 90% smectite layers, and R1 M-L I/S 30S, randomly ordered mixed-layer illite/smectite with 30% smectite layers.

Sample Depth (ft)	Well Name	Qtz	K-spar	Plag	Ank	Cal	Dol	Pyr	Gyp	R0	R1	Illite & Mica	Kao	Chlor
1840-1845	GO1A	83.5	0.2	2.4	2.6	3.5	1.2	-	-	-	-	2.2	1.2	3.2
1845-1850	GO1A	70.6	0.3	2.3	1.9	14.6	2.6	-	-	-	-	3.6	1.0	3.1
1850-1855	GO1A	84.2	0.3	4.1	1.1	3.4	0.5	-	-	-	-	2.7	1.6	2.1
1795-1800	GH3	85.4	0.5	3.1	-	1.7	1.2	-	-	-	-	1.7	1.6	4.8
1800-1805	GH3	79.5	0.4	3.9	0.8	3.5	-	-	-	-	-	3.9	2.6	5.4
1810-1815	GH3	79.7	0.3	3.7	1.5	5.1	0.3	-	-	-	-	2.9	2.4	4.1
*1810-1815	TB1	25.7	2.4	3.3	1.9	5.9	-	0.6	-	18.5	16.7	18.8	2.7	3.5
1815-1820	TB1	79.3	0.3	1.5	14.3	0.6	-	-	-	-	-	2.2	1.8	-
1820-1825	TB1	80.4	0.3	1.9	12.8	0.4	-	0.2	-	-	-	2.0	2.0	-
*1780-1785	WT2	25.7	2.4	1.8	1.7	8.8	-	0.5	0.4	18.7	15.9	16.2	4.4	3.5
1785-1790	WT2	74.1	0.3	2.6	17.6	0.9	-	0.2	-	-	-	2.1	2.2	-
1790-1795	WT2	75.1	0.2	2.3	12.9	0.7	-	0.3	-	-	-	3.4	3.2	1.9
1795-1800	WT2	87.6	0.2	3.0	1.3	1.2	-	0.1	-	-	-	2.2	2.7	1.7
*1730-1735	WT2	28.6	2.6	2.9	1.9	19.4	-	0.4	-	2.2	17.6	17.9	3.6	2.9
1735-1740	DL1	78.0	0.3	1.4	15.8	0.4	-	0.2	-	-	-	2.1	1.8	-
1740-1745	DL1	78.4	0.2	4.2	1.7	0.7	-	-	-	-	-	3.7	6.5	4.6
1740-1745	DL1	89.5	0.2	2.9	2.1	0.3	-	-	-	-	-	2.1	2.6	0.3

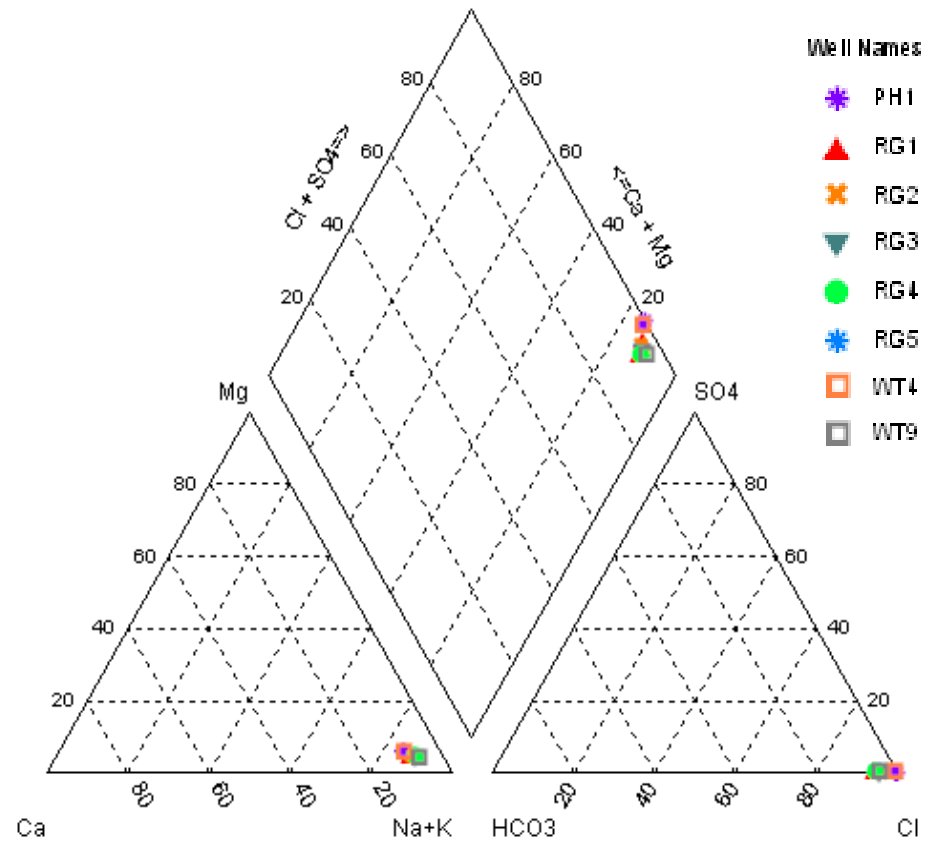


Figure 4.1 Piper plot showing major-ion concentrations in Jackson formation water samples collected before CO₂ injection.

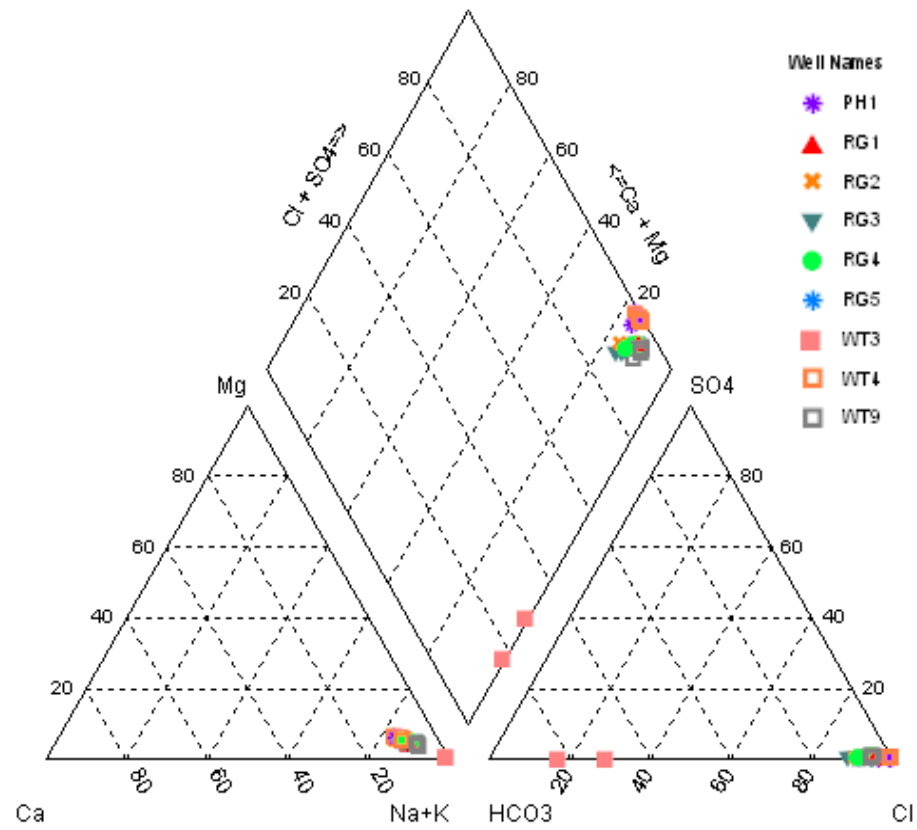


Figure 4.2 Piper plot showing major-ion concentrations for Jackson formation water samples collected during CO₂ injection.

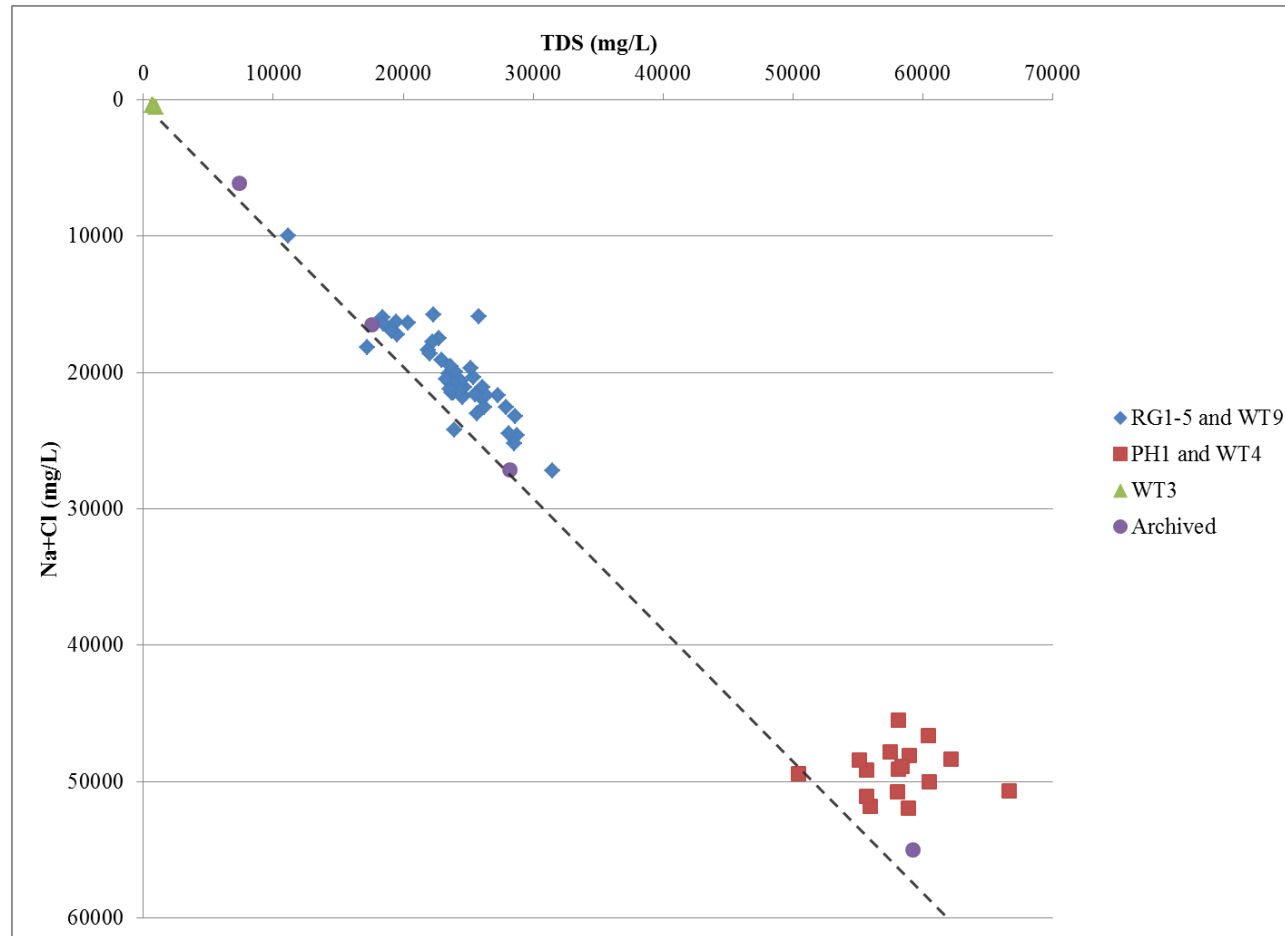


Figure 4.3 Sodium chloride (Na+Cl) versus TDS for Jackson and Pennsylvanian (WT3) formation water samples. Compartmentalization in the reservoir is evidenced by the distinct separation between RG1-5, WT9 and PH1, WT4. The four archived samples were collected from other oil fields near Sugar Creek. The dashed line represents a line of best fit for the archived data, creating a historic trend line for pristine Mississippian formation water in the Jackson.

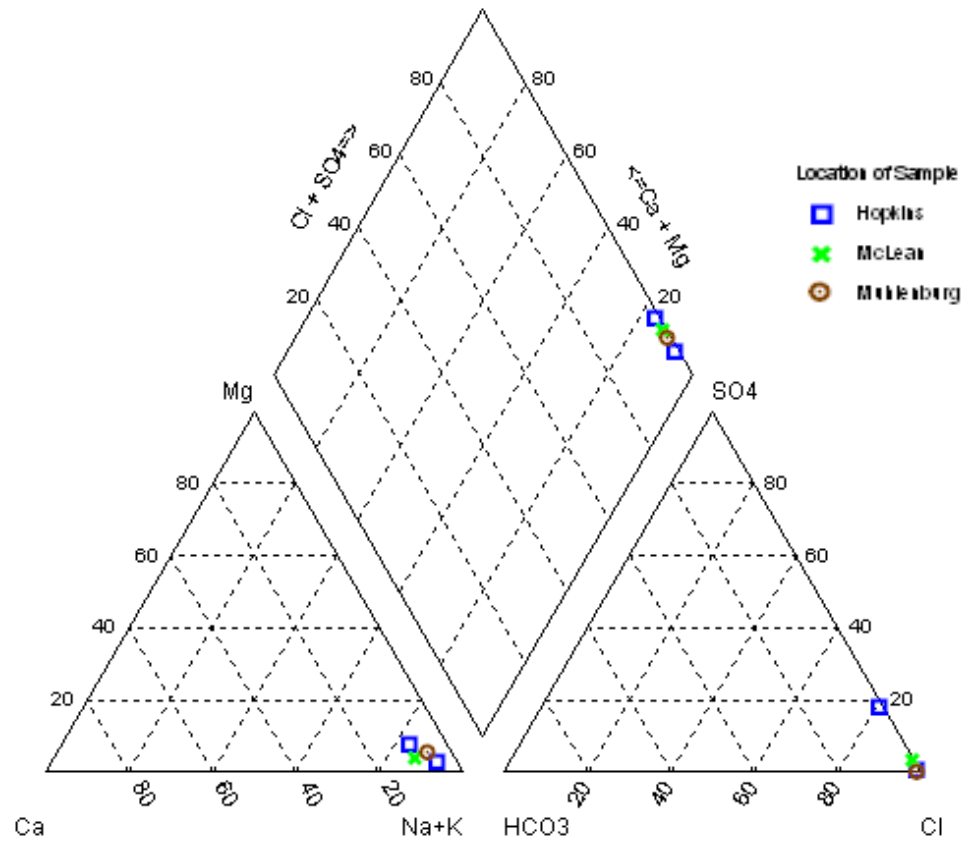


Figure 4.4 Piper plot showing major-ion concentrations for archived Jackson formation water from fields near Sugar Creek.

Chapter 5: GWB Modeling Results

In order to simulate injection of CO₂ into the Jackson reservoir and seal rocks, a mixture of GWB model types (speciation, path of reaction, and kinetic reaction) were used. The models were tailored to fit reservoir temperature and pressure conditions, baseline CO₂ concentrations, injection pressures, and formation-water chemistry. The models for seal rocks and reservoir rocks were separated due to different porosity and mineralogy. As the models were run under conditions of constant temperature equal to 28°C (82°F), the principal variable in the geochemical modeling process was CO₂ fugacity ($f\text{CO}_2$), which represented the variation in pressure and CO₂ concentration in the reservoir and seal rocks throughout the injection process (Tables 5.1a,b). As described in the Methods section, measured reservoir pressure and CO₂ concentration at the injection well and production wells allowed the spatial variation in $f\text{CO}_2$ in the field to be calculated. Simulations were run in which the highest $f\text{CO}_2$ coincided with the injection well and the lowest with the production well. An important aspect of GWB modeling is accounting for the effect of salinity on CO₂ solubility and modifying the database to correct for this salting-out effect. Ignoring these effects overestimates the long-term CO₂ trapping through carbonate mineral precipitation, especially in formation waters with high TDS values (Allen, 2005; Zerai, 2006).

Conceptually, the modeling process was split into distinct phases representing the variation in $f\text{CO}_2$ and reservoir chemistry before, during, and after injection. The configuration of GWB required that the pre-, post-, and injection phases be simulated in four steps. The four phases included: 1) pre-CO₂ injection, 2) CO₂ injection phase I, 3) CO₂ injection phase II, and 4) post-CO₂ injection. The pre-injection phase was simulated

using an equilibrium, or speciation, model in which baseline CO_2 and CH_4 concentrations, as measured in the field and laboratory, were brought into equilibrium with formation water. The results from the pre-injection phase were "picked-up" in GWB and used as the starting point for injection phase I simulation. Injection phase I involved raising $f\text{CO}_2$ to represent CO_2 injection but with no minerals included. Results from injection phase I were again "picked-up" in GWB and used as the starting conditions for simulating injection phase II, in which kinetic minerals were titrated into the system for 365 days, representing the approximate CO_2 injection period for Sugar Creek. Notably, injection phase II was the only simulation step in which time was an explicit variable because the kinetic minerals are partly defined by rate constants. All other simulation steps in which a reaction path was followed (that is, steps 1, 2 and 4) were discriminated against the dimensionless reaction progress. The fourth, or post-injection phase, involved sliding the $f\text{CO}_2$ back down to the pre-injection value. Before reducing $f\text{CO}_2$, minerals that equilibrated during injection phase II were swapped into the basis, which provided the opportunity to simulate how minerals reacted in the post- CO_2 injection phase.

Within the model, important variables that remained constant throughout the simulations include porosity, temperature, and water saturation. Quantitative outputs from the GWB steps are separated into seal and reservoir rocks at the injection well, mid-point fugacity, and production wells. The results include $f\text{CO}_2$ and carbonate equilibrium, mineral saturation (log Q/K values, Tables 5.2a-d), and the masses of reacted minerals (Tables 5.3a-d).

5.1 Pre-CO₂ Injection

Based on field measurements of gas composition and pressure, the highest CO₂ concentrations, and hence $f\text{CO}_2$, are associated with the injection and mid-point fugacity wells ($f\text{CO}_2 = 1.3$), and lowest CO₂ concentration and $f\text{CO}_2$ with the production wells ($f\text{CO}_2 = 0.071$, Tables 5.1a,b). Speciation modeling using these CO₂ fugacities and the water chemistry mentioned in Chapter 4 shows the highest aqueous CO₂ concentrations occur at the injection well with slightly lower values at the mid-fugacity and production wells. According to field measurements, the highest alkalinities were at the injection well (689 mg/kg) and RG1-4, WT9 (557-920 mg/kg). Lowest alkalinities are associated with PH1, WT4 (310-352 mg/kg). Speciation modeling done for the pre-CO₂ injection phase supports the alkalinity distribution found in the field, but with higher values. Simulated pH values equal 5.6 in the injection and mid-point fugacity wells, which is about 1.5 pH units lower than measured at RG5 (Figure 5.1). Simulated pH values for RG1-4, WT9 and PH1, WT4 equal 6.1 and 6.5, respectively. These values are also less than values measured in the field by 0.5 to 1 pH unit. At RG5, the water is highly undersaturated with respect to all of the alumino-silicate minerals (i.e. K-feldspar, plagioclase), slightly undersaturated (close to equilibrium) with respect to calcite, dolomite and quartz, and supersaturated with respect to pyrite (Table 5.2a). Results for the mid-fugacity well are similar but the magnitude of undersaturation and saturation was diminished or increased, respectively (Table 5.2b). In contrast, log Q/K values for RG1-4, WT9 show supersaturation with respect to alumino-silicate minerals except for chlorite, which remains undersaturated; near-equilibrium conditions for quartz; slight undersaturation for calcite and dolomite; and supersaturation for pyrite (Table 5.2c). PH1, WT4 shows even

higher degrees of supersaturation for the alumino-silicate minerals; slight super saturation for calcite, dolomite, and quartz (which is very close to equilibrium); and supersaturation for pyrite (Table 5.2d).

5.2 CO₂ Injection Phase I

During injection phase I, $f\text{CO}_2$ (based on injection pressure and CO₂ concentration) is raised to simulate injection of CO₂ into the reservoir. Tables 5.1a and 5.1b show that $f\text{CO}_2$ is highest at RG5 (49.6 bars), intermediate at the mid-point fugacity (25.6 bars), and lowest at production wells (1.68 bars). The elevated $f\text{CO}_2$ produces corresponding increases in aqueous CO₂ (Tables 5.1a,b). The increased aqueous CO₂ reduces pH to values in the lower 4 range at RG5 and mid-point fugacity, and values in the lower to mid-5 range for the production wells (Figure 5.1). The pH of formation water in the reservoir and seal rocks was similar, but pH values in the latter were approximately a tenth of a pH unit lower as compared to the former. Relative to pre-CO₂ injection values, the fluid response to CO₂ injection shows a decrease in carbonate alkalinity by more than half at RG5 (1050 to 514 mg/kg), a moderate decrease at the mid-point fugacity (795 to 504 mg/kg), and a smaller decrease (704 to 648 mg/kg) at the production wells (Figure 5.2). Differences between aqueous fluid properties at RG1-4, WT9 and PH1, WT4 are a reflection of differences in the pre-CO₂ injection water chemistry caused by the operational water flood and reservoir compartmentalization.

As compared to the pre-CO₂ injection phase, mineral saturation values decrease for most minerals such that most are undersaturated at the end of the phase. Results for saturation states show varying degrees of supersaturation for pyrite (log Q/K range of

1.43 to 8.41). Quartz is near equilibrium, and water in the reservoir rock is undersaturated with respect to calcite, dolomite, K-feldspar, chlorite and albite (Tables 5.2a-d). The decrease in saturation states is especially apparent in PH1, WT4 where minerals that were saturated (e.g. calcite, dolomite, k-feldspar, albite) before CO₂ injection are undersaturated after simulating CO₂ injection phase I (Table 5.2d). Spatially, the degree of undersaturation progressively decreases going from the injection, mid-fugacity, and production wells. Among the production well simulations, however, the degree of undersaturation was greatest for PH1, WT4 as compared to RG1-4, WT9 wells.

5.3 CO₂ Injection Phase II

The elevated $f\text{CO}_2$ values established in CO₂ injection phase I are retained in CO₂ injection phase II, in which the kinetic minerals are titrated into the aqueous fluid. The results at the end of CO₂ injection phase II are important because they include the complete geochemical system of interest; that is, the aqueous fluid with elevated $f\text{CO}_2$, and the reservoir and seal rock minerals (treated kinetically).

When the kinetic minerals are titrated in during CO₂ injection phase II, the aqueous fluid responds with a rapid increase (less than one day) in pH as compared to values in the previous phase (Figure 5.3). The pH values at the end of the 365 day mineral titration range from 4.9 at RG5 to 5.7 at RG1-4, WT9; similarly, alkalinity values range from 3378 mg/kg at RG5 to 804 mg/kg at RG1-4, WT9 and are higher than in CO₂ injection phase I (Table 5.1a, Figure 5.1). Spatially, the magnitude of change in pH and alkalinity values decreases the farther away from the injection well. The response of the

seal rocks at the end of CO₂ injection phase II was similar to the response in the reservoir rocks, but the magnitude of change was less.

Changes in mineral saturation provide the geochemical driver for precipitation and dissolution as minerals are titrated into the CO₂-rich, low pH formation waters. Mineral saturations change rapidly, within days of kinetic mineral titration. With the exception of pyrite, for which saturation decreases from super-saturation to equilibrium, all reservoir and seal mineral saturation states increase (Tables 5.2a-d). Carbonate minerals go to equilibrium quickly from previous conditions of supersaturation (e.g. dolomite at PH1, WT4 and RG1-4, WT9) and undersaturation (e.g. calcite at RG5, mid-fugacity, RG1-4, WT9). Following CO₂-injection phase II, feldspar is undersaturated for most reservoir and seal rocks, except albite, which is at equilibrium in the seal rocks at RG5.

Minerals precipitating at RG5 and the mid-point fugacity within the reservoir include gibbsite, strontianite, and witherite (Table 5.3b). The RG1-4, WT9 wells show gibbsite, strontianite, witherite, and muscovite precipitating and PH1, WT4 wells show strontianite, witherite, siderite, and muscovite (Table 5.3b). Within the seal rocks, the minerals precipitating at RG5 and the mid-point fugacity during the second injection phase include gibbsite, strontianite, and barite (Table 5.3d). Mineral precipitation in seal rocks at RG1-4, WT9 and PH1, WT4 wells includes: strontianite, barite, and muscovite (Table 5.3d). GWB predicts that approximately 5.5 grams of calcite dissolve rapidly (within one day of titration) into the system at RG5, mid-point fugacity (Figure 5.4), and PH1, WT4, and only 2.3 grams dissolve at RG1-4, WT9. Conversely, the highest amount of dolomite rapidly precipitates into the system at PH1, WT4 (3.8 grams), a moderate

amount at mid-point fugacity (1.4 grams, Figure 5.5) and RG1-4, WT9 (1.1 grams), and the lowest at the injection well (0.4 grams). Over all change in mineral mass versus time shows a net dissolution mass change with carbonate minerals (calcite, dolomite and strontianite) as the dominantly controlling minerals which represent the largest change in mass (Figure 5.6).

5.4 Post-CO₂ Injection Phase

The $f\text{CO}_2$ is reduced down to pre-injection values during the post-CO₂ injection phase using a sliding fugacity model, and requires minerals that equilibrated with formation water during the previous phase to be swapped into the basis. For example, dolomite is substituted for Mg^{+2} , calcite for Ca^{+2} , strontianite for Sr^{+2} , gibbsite for Al^{+3} , and pyrite for Fe^{+2} . The simulation proceeds along a non-dimensional reaction path as $f\text{CO}_2$ is reduced.

Results show increasing pH for the formation water in the reservoir rocks, with the largest increase at RG5 (about 1 pH unit), moderate increase for mid-point fugacity and RG1-4, WT9 (about 0.75 pH unit) and the lowest increase at PH1, WT4 (about 0.7 pH unit, Figure 5.1). Carbonate alkalinity decreases and HCO_3^- species are predicted to decrease by an order of magnitude as $f\text{CO}_2$ is decreased. The largest decrease in carbonate alkalinity for reservoir rocks is at RG5 (3739 to 1744 mg/kg), with moderate decreases at mid-point fugacity (2899 to 1264 mg/kg) and RG1-4, WT9 (1063 to 332 mg/kg), and the lowest decrease at PH1, WT4 (903 to 269 mg/kg, Figure 5.2). Formation water in the seal rock shows similar increases in pH and decreases in alkalinity as that in the reservoir. Final pH values in seal rock formation water are slightly less than that in the reservoir

and alkalinities show the same but with a greater magnitude of difference (Tables 5.1a, 5.1b).

Predicted mineral saturation values show the carbonate minerals to be at equilibrium in the reservoir and seal rock simulations (Tables 5.2a-d). The saturation state of quartz in the post-CO₂ injection phase decreases from the preceding simulation phase such that it is undersaturated in the reservoir rock simulations, except for PH1, WT4, where it is at equilibrium. In contrast, quartz attains equilibrium in all of the seal rock simulations. The feldspars are undersaturated in the reservoir and seal rock simulations for all wells, with the exception of albite at RG5 in the seal rock. The only example of where a clay species, kaolinite, is at equilibrium is for the seal rocks at RG5. At the remaining wells, the clay minerals were undersaturated in the post-CO₂ injection phase (Tables 5.2a-d).

During the post-CO₂ injection phase, minerals precipitating at RG5, the mid-point fugacity, and RG1-4, WT9 wells include calcite, dolomite, gibbsite, kaolinite, pyrite, strontianite, and witherite (Tables 5.3a-d). At the PH1, WT4 wells, calcite, dolomite, kaolinite, pyrite, strontianite, witherite, quartz and siderite precipitate (Tables 5.3a-d). Over-all change in mineral mass in grams versus time shows net precipitation, with calcite, dolomite and strontianite as the dominantly controlling minerals (Figure 5.7).

Table 5.1a Variation in calculated $f\text{CO}_2$ during the four GWB simulation phases at different wells for Jackson formation waters in the reservoir. Changes in $f\text{CO}_2$ produce changes in aqueous CO_2 , HCO_3^- , carbonated alkalinity, and pH.

Sugar Creek Reservoir Rocks		Pre-injection	Injection Phase I	Injection Phase II	Post-injection	
Decreasing CO_2 fugacity	Injection well	$f\text{CO}_2$ (bar)	1.3	49.6	49.6	1.3
		CO_2 (aq) (molal)	0.04334	1.657	1.657	0.04343
		pH (<i>measured/modeled</i>)	7.187/5.616	4.038	4.903	5.857
		Carbonate alkalinity (mg/kg)	1050	514	3739	1744
		HCO_3^- (molality)	0.01066	0.01077	0.07997	0.01862
	Mid-point fugacity	$f\text{CO}_2$ (bar)	1.3	25.6	25.6	1.3
		CO_2 (aq) (molal)	0.04273	0.8552	0.8552	0.04343
		pH (<i>measured/modeled</i>)	6.379/5.591	4.293	5.054	5.795
		Carbonate alkalinity (mg/kg)	795	504	2899	1264
		HCO_3^- (molality)	0.01013	0.01021	0.05919	0.01647
	Production wells (RG1-4/WT9)	$f\text{CO}_2$ (bar)	0.071	1.68	1.68	0.071
		CO_2 (aq) (molal)	0.01787	0.05612	0.05612	0.002372
		pH (<i>measured/modeled</i>)	6.418/6.053	5.558	5.765	6.515
		Carbonate alkalinity (mg/kg)	704	648	1063	332
		HCO_3^- (molality)	0.01212	0.01218	0.01962	0.004653
	Production wells (PH1/WT4)	$f\text{CO}_2$ (bar)	0.071	1.68	1.68	0.071
		CO_2 (aq) (molal)	0.002386	0.05612	0.05612	0.002372
		pH (<i>measured/modeled</i>)	6.823/6.518	5.165	5.673	6.385
		Carbonate alkalinity (mg/kg)	365	262	903	269
		HCO_3^- (molality)	0.004813	0.00503	0.01621	0.003526

Table 5.1b Variation in calculated $f\text{CO}_2$ during the four GWB simulation phases at different wells for Jackson formation waters in the seal rocks. Changes in $f\text{CO}_2$ produce changes in aqueous CO_2 , HCO_3^- , carbonated alkalinity, and pH.

Sugar Creek Seal Rocks		Pre-injection	Injection Phase I	Injection Phase II	Post-injection	
Decreasing CO_2 fugacity ↓	Injection well	$f\text{CO}_2$ (bar)	1.3	49.6	49.6	1.3
		CO_2 (aq) (molal)	0.04334	1.657	1.657	0.04343
		pH (<i>measured</i> /modeled)	7.187/5.616	4.038	4.858	5.734
		Carbonate alkalinity (mg/kg)	1050	514	3378	751
		HCO_3^- (molality)	0.01066	0.01077	0.07261	0.01418
	Mid-point fugacity	$f\text{CO}_2$ (bar)	1.3	25.6	25.6	1.3
		CO_2 (aq) (molal)	0.04273	0.8552	0.8552	0.04343
		pH (<i>measured</i> /modeled)	6.379/5.591	4.293	5.002	5.700
		Carbonate alkalinity (mg/kg)	795	504	2553	713
		HCO_3^- (molality)	0.01013	0.01021	0.05277	0.01332
	Production wells (RG1-4/WT9)	$f\text{CO}_2$ (bar)	0.071	1.68	1.68	0.071
		CO_2 (aq) (molal)	0.01787	0.05612	0.05612	0.002338
		pH (<i>measured</i> /modeled)	6.418/6.053	5.558	5.651	6.365
		Carbonate alkalinity (mg/kg)	704	648	804	193
		HCO_3^- (molality)	0.01212	0.01218	0.01525	0.003283
	Production wells (PH1/WT4)	$f\text{CO}_2$ (bar)	0.071	1.68	1.68	0.071
		CO_2 (aq) (molal)	0.002386	0.05612	0.05612	0.002372
		pH (<i>measured</i> /modeled)	6.823/6.518	5.165	5.598	6.299
		Carbonate alkalinity (mg/kg)	365	262	740	187
		HCO_3^- (molality)	0.004813	0.00503	0.01365	0.002896

Table 5.2a Mineral saturation (log Q/K) values for minerals during each of the four GWB simulation phases at RG5 (injection well). GWB describes the saturation state of minerals with real numbers only for minerals with log Q/K greater than -3. Values greater than zero are super-saturated, equal to zero are at equilibrium, and less than zero are undersaturated. #Represents the saturation state for dolomite, and is a proxy for ankerite, which lacks thermodynamic data in GWB. *Denotes new minerals that precipitate in the system.

	Mineral	Pre-injection	Injection phase I	Injection phase II	Post-injection
Reservoir Rocks	Quartz	-0.0335	-0.0334	0.00	-0.2624
	Calcite	-0.8142	-2.3879	0.00	0.00
	#Dolomite	-0.7185	≤ -3.0	0.00	0.00
	Chlorite	≤ -3.0	≤ -3.0	≤ -3.0	≤ -3.0
	Pyrite	4.1414	1.4342	0.00	0.00
	K-feldspar	≤ -3.0	≤ -3.0	-2.4688	-2.4954
	Albite	≤ -3.0	≤ -3.0	-2.6519	-2.6645
	*Strontianite	1.4909	-0.0829	0.00	0.00
	*Witherite	1.1996	-0.3740	0.00	0.00
Seal Rocks	Quartz	Log Q/K values seal are the same as reservoir rocks in pre-injection and injection phase I		0.1620	0.00
	Calcite			0.00	0.00
	#Dolomite			0.00	0.00
	Chlorite			≤ -3.0	≤ -3.0
	Pyrite			0.00	0.00
	K-feldspar			-2.1535	-1.5740
	Albite			0.00	0.00
	Barite	≤ -3.0	≤ -3.0	-2.4219	-2.2773
	Illite	≤ -3.0	≤ -3.0	-2.2207	-2.1989
	Kaolinite	≤ -3.0	≤ -3.0	0.8486	0.00
	Gypsum	≤ -3.0	≤ -3.0	0.00	-0.0608

Table 5.2b Mineral saturation (log Q/K) values for minerals during each of the four GWB simulation phases at the mid-fugacity. GWB describes the saturation state of minerals with real numbers only for minerals with log Q/K greater than -3. Values greater than zero are super-saturated, equal to zero are at equilibrium, and less than zero are undersaturated. #Represents the saturation state for dolomite, and is a proxy for ankerite, which lacks thermodynamic data in GWB. *Denotes new minerals that precipitate in the system.

	Mineral	Pre-injection	Injection phase I	Injection phase II	Post-injection
Reservoir Rocks	Quartz	-0.0161	-0.0160	0.0674	-0.2636
	Calcite	-0.6982	-1.9930	-0.00	0.00
	#Dolomite	-0.4730	≤ -3.0	0.00	0.00
	Chlorite	≤ -3.0	≤ -3.0	≤ -3.0	≤ -3.0
	Pyrite	7.3726	5.1529	0.00	0.00
	K-feldspar	-0.2828	≤ -3.0	-2.1312	-2.3791
	Albite	-0.4389	≤ -3.0	-2.3254	-2.5641
	*Strontianite	1.6014	0.3065	0.00	0.00
	*Witherite	1.1654	-0.1293	0.00	0.00
Seal Rocks	Quartz	Log Q/K values seal are the same as reservoir rocks in pre-injection and injection phase I		0.1620	0.00
	Calcite			0.00	0.00
	#Dolomite			0.0001	0.00
	Chlorite			≤ -3.0	≤ -3.0
	Pyrite			0.0001	0.00
	K-feldspar			-1.5881	-1.5566
	Albite			-2.1014	-2.1428
	Barite	≤ -3.0	≤ -3.0	0.00	0.00
	Illite	1.7514	≤ -3.0	-1.8060	-2.1868
	Kaolinite	3.6657	-2.4096	0.8509	0.00
	Gypsum	≤ -3.0	≤ -3.0	-0.0002	-0.0473

Table 5.2c Mineral saturation (log Q/K) values for minerals during each of the four GWB simulation phases at RG1-4/WT9. GWB describes the saturation state of minerals with real numbers only for minerals with log Q/K greater than -3. Values greater than zero are super-saturated, equal to zero are at equilibrium, and less than zero are undersaturated. #Represents the saturation state for dolomite, and is a proxy for ankerite, which lacks thermodynamic data in GWB. *Denotes new minerals that precipitate in the system.

	Mineral	Pre-injection	Injection phase I	Injection phase II	Post-injection
Reservoir Rocks	Quartz	-0.0069	-0.0066	0.0653	-0.2628
	Calcite	-0.2609	-0.7540	0.00	0.00
	#Dolomite	0.3794	-0.6067	0.00	0.00
	Chlorite	≤ -3.0	≤ -3.0	≤ -3.0	≤ -3.0
	Pyrite	8.5326	7.7624	0.00	0.00
	K-feldspar	0.3720	-0.4237	-1.4830	-1.7138
	Albite	0.1676	-0.6281	-1.7202	-1.9482
	*Strontianite	2.2388	1.7457	0.00	0.00
	*Witherite	1.6652	1.1721	0.00	0.00
Seal Rocks	Quartz	Log Q/K values seal are the same as reservoir rocks in pre-injection and injection phase I		0.1620	0.00
	Calcite			-0.00	0.00
	#Dolomite			0.00	0.00
	Chlorite			≤ -3.0	≤ -3.0
	Pyrite			0.0001	0.00
	K-feldspar			-1.4575	-0.9574
	Albite			-1.5688	-1.5873
	Barite	≤ -3.0	≤ -3.0	0.00	0.00
	Illite	2.7447	1.5077	-1.4559	-1.5113
	Kaolinite	4.1399	3.5375	0.8240	0.00
	Gypsum	≤ -3.0	≤ -3.0	-0.00	-0.0340

Table 5.2d Mineral saturation (log Q/K) values for minerals during each of the four GWB simulation phases at PH1/WT4. GWB describes the saturation state of minerals with real numbers only for minerals with log Q/K greater than -3. Values greater than zero are super-saturated, equal to zero are at equilibrium, and less than zero are undersaturated. #Represents the saturation state for dolomite, and is a proxy for ankerite, which lacks thermodynamic data in GWB. *Denotes new minerals that precipitate in the system.

	Mineral	Pre-injection	Injection phase I	Injection phase II	Post-injection
Reservoir Rocks	Quartz	0.0227	0.0251	0.0425	0.00
	Calcite	0.0624	-1.2709	-0.00	0.00
	#Dolomite	1.1182	-1.5484	0.00	0.00
	Chlorite	≤ -3.0	≤ -3.0	≤ -3.0	≤ -3.0
	Pyrite	10.4092	8.4131	-0.00	0.00
	K-feldspar	1.2253	-1.0182	-1.4549	-1.0543
	Albite	1.1143	-1.1292	-1.5235	-1.1808
	*Strontianite	1.9332	0.5998	0.00	0.00
	*Witherite	1.7706	0.4374	0.00	0.00
Seal Rocks	Quartz	Log Q/K values seal are the same as reservoir rocks in pre-injection and injection phase I		0.1620	0.00
	Calcite			-0.00	0.00
	#Dolomite			0.0001	0.00
	Chlorite			≤ -3.0	≤ -3.0
	Pyrite			-0.00	0.00
	K-feldspar			-1.2894	-0.9650
	Albite			-1.3298	-1.2747
	Barite	≤ -3.0	≤ -3.0	-0.00	0.00
	Illite	3.6660	0.1206	-1.4991	-1.5120
	Kaolinite	4.2357	2.4438	0.6484	0.00
	Gypsum	≤ -3.0	≤ -3.0	-0.00	-0.0219

Table 5.3a Simulated mineral precipitation and dissolution for reservoir rocks. Positive values are precipitation and negative equal dissolution. *Represents dolomite and ankerite. Abbreviations: “nc” equals no change in mass or volume and “na” indicates mineral did not precipitate for simulation.

Starting Reservoir Minerals		Injection Step II		Post-Injection	
		Mass (g)	Volume (cm ³)	Mass (g)	Volume (cm ³)
Calcite	RG5	-5.42	2.0	3.57	1.32
	Mid-point	-5.49	2.0	2.62	0.97
	RG1-4/WT9	-2.33	0.86	0.83	0.31
	PH1/WT4	-5.34	1.97	0.88	0.33
*Dolomite	RG5	0.41	0.14	0.56	0.20
	Mid-point	1.38	0.48	0.39	0.14
	RG1-4/WT9	1.15	0.4	0.13	0.04
	PH1/WT4	3.82	1.33	0.12	0.04
Quartz	RG5	0.08	0.03	nc	nc
	Mid-point	0.08	0.03	nc	nc
	RG1-4/WT9	0.08	0.03	nc	nc
	PH1/WT4	0.05	0.02	<-0.01	<-0.01
K-feldspar	RG5	<-0.01	<0.01	nc	nc
	Mid-point	<-0.01	<0.01	nc	nc
	RG1-4/WT9	<-0.01	<0.01	nc	nc
	PH1/WT4	<-0.01	<0.01	nc	nc
Albite	RG5	-0.1	0.04	nc	nc
	Mid-point	-0.1	0.04	nc	nc
	RG1-4/WT9	-0.09	0.04	nc	nc
	PH1/WT4	-0.09	0.04	nc	nc
Illite	RG5	-0.01	0.01	nc	nc
	Mid-point	-0.01	0.01	nc	nc
	RG1-4/WT9	-0.01	<0.01	nc	nc
	PH1/WT4	-0.01	<0.01	nc	nc
Kaolinite	RG5	<0.01	<0.01	<0.01	<0.01
	Mid-point	<0.01	<0.01	<0.01	<0.01
	RG1-4/WT9	<0.01	<0.01	<0.01	<0.01
	PH1/WT4	<0.01	<0.01	0.07	0.03
Chlorite	RG5	-0.01	0.01	nc	nc
	Mid-point	-0.01	0.01	nc	nc
	RG1-4/WT9	-0.01	0.01	nc	nc
	PH1/WT4	-0.01	0.01	nc	nc
Pyrite	RG5	<0.01	<0.01	<0.01	<0.01
	Mid-point	<0.01	<0.01	<0.01	<0.01
	RG1-4/WT9	<0.01	<0.01	<0.01	<0.01
	PH1/WT4	0.01	0.01	<0.01	<0.01

Table 5.3b New minerals precipitated in response to CO₂ injection and not part of the original reservoir mineralogy in reservoir rocks. Abbreviations: “nc” equals no change in mass or volume and “na” indicates mineral did not precipitate for simulation.

Starting Reservoir Minerals		CO ₂ -Injection phase II		Post-CO ₂ Injection	
		Mass (g)	Volume (cm ³)	Mass (g)	Volume (cm ³)
Gibbsite	RG5	0.04	0.02	0.03	0.01
	Mid-point	0.04	0.02	0.03	0.01
	RG1-4/WT9	0.04	0.02	0.03	0.01
	PH1/WT4	na	na	na	na
Strontianite	RG5	0.46	0.12	0.47	0.13
	Mid-point	0.79	0.21	0.8	0.21
	RG1-4/WT9	0.92	0.24	0.92	0.24
	PH1/WT4	0.5	0.13	0.5	0.13
Witherite	RG5	<0.01	<0.01	<0.01	<0.01
	Mid-point	<0.01	<0.01	<0.01	<0.01
	RG1-4/WT9	<0.01	<0.01	<0.01	<0.01
	PH1/WT4	<0.01	<0.01	<0.01	<0.01
Siderite	PH1/WT4	0.03	0.01	0.04	0.01

Table 5.3c Simulated mineral precipitation and dissolution for seal rocks. Positive values are precipitation and negative equal dissolution. *Represents dolomite and ankerite. Abbreviations: “nc” equals no change in mass or volume and “na” indicates mineral did not precipitate for simulation.

Starting Seal Minerals		CO ₂ -Injection phase II		Post-CO ₂ Injection	
		Mass (g)	Volume (cm ³)	Mass (g)	Volume (cm ³)
Calcite	RG5	2.27	0.84	3.2	1.18
	Mid-point	0.97	0.36	2.32	0.86
	RG1-4/WT9	-1.42	0.52	0.7	0.26
	PH1/WT4	-4.6	1.7	0.81	0.3
Dolomite*	RG5	0.18	0.06	0.51	0.18
	Mid-point	1.12	0.39	0.35	0.12
	RG1-4/WT9	0.73	0.26	0.11	0.04
	PH1/WT4	3.42	1.20	0.11	0.04
Quartz	RG5	0.16	0.06	-0.09	0.03
	Mid-point	0.16	0.06	-0.08	0.03
	RG1-4/WT9	0.16	0.06	-0.07	0.03
	PH1/WT4	0.16	0.06	-0.07	0.03
K-feldspar	RG5	-0.14	0.05	nc	nc
	Mid-point	-0.13	0.05	nc	nc
	RG1-4/WT9	-0.13	0.06	nc	nc
	PH1/WT4	-0.13	0.05	nc	nc
Albite	RG5	-0.2	0.08	nc	nc
	Mid-point	-0.2	0.08	nc	nc
	RG1-4/WT9	-0.2	0.08	nc	nc
	PH1/WT4	-0.19	0.07	nc	nc
Illite	RG5	-0.48	0.18	nc	nc
	Mid-point	-0.48	0.17	nc	nc
	RG1-4/WT9	-0.47	0.17	nc	nc
	PH1/WT4	-0.47	0.17	nc	nc
Kaolinite	RG5	0.01	0.01	0.55	0.21
	Mid-point	0.01	<0.01	0.54	0.21
	RG1-4/WT9	0.01	<0.01	-0.45	0.17
	PH1/WT4	<0.01	<0.01	-0.36	0.14
Chlorite	RG5	-0.05	0.02	nc	nc
	Mid-point	-0.05	0.02	nc	nc
	RG1-4/WT9	<-0.01	<-0.01	nc	nc
	PH1/WT4	-0.05	0.02	nc	nc
Gypsum	RG5	-16.84	7.31	<-0.01	<-0.01
	Mid-point	-11.97	5.19	-0.03	0.01
	RG1-4/WT9	-6.29	2.73	nc	nc
	PH1/WT4	-7.56	3.28	nc	nc

Table 5.3d New minerals precipitated in response to CO₂ injection and not part of the original mineralogy in seal rocks. Abbreviations: “nc” equals no change in mass or volume and “na” indicates mineral did not precipitate for simulation.

New Seal Minerals		CO ₂ -injection phase II		Post-CO ₂ injection phase	
		Mass (g)	Volume (cm ³)	Mass (g)	Volume (cm ³)
Gibbsite	RG5	0.08	0.03	nc	nc
	Mid-point	0.25	0.1	nc	nc
	RG1-4/WT9	na	na	na	na
	PH1/WT4	na	na	na	na
Strontianite	RG5	0.46	0.12	0.47	0.12
	Mid-point	0.78	0.21	0.79	0.21
	RG1-4/WT9	0.91	0.24	0.91	0.24
	PH1/WT4	0.49	0.13	0.5	0.13
Barite	RG5	<0.01	<0.01	<0.01	<0.01
	Mid-point	<0.01	<0.01	<0.01	<0.01
	RG1-4/WT9	<0.01	<0.01	<0.01	<0.01
	PH1/WT4	<0.01	<0.01	<0.01	<0.01
Alunite	RG5	0.45	0.32	nc	nc
	Mid-point	0.13	0.09	nc	nc
	RG1-4/WT9	na	na	na	na
	PH1/WT4	na	na	na	na

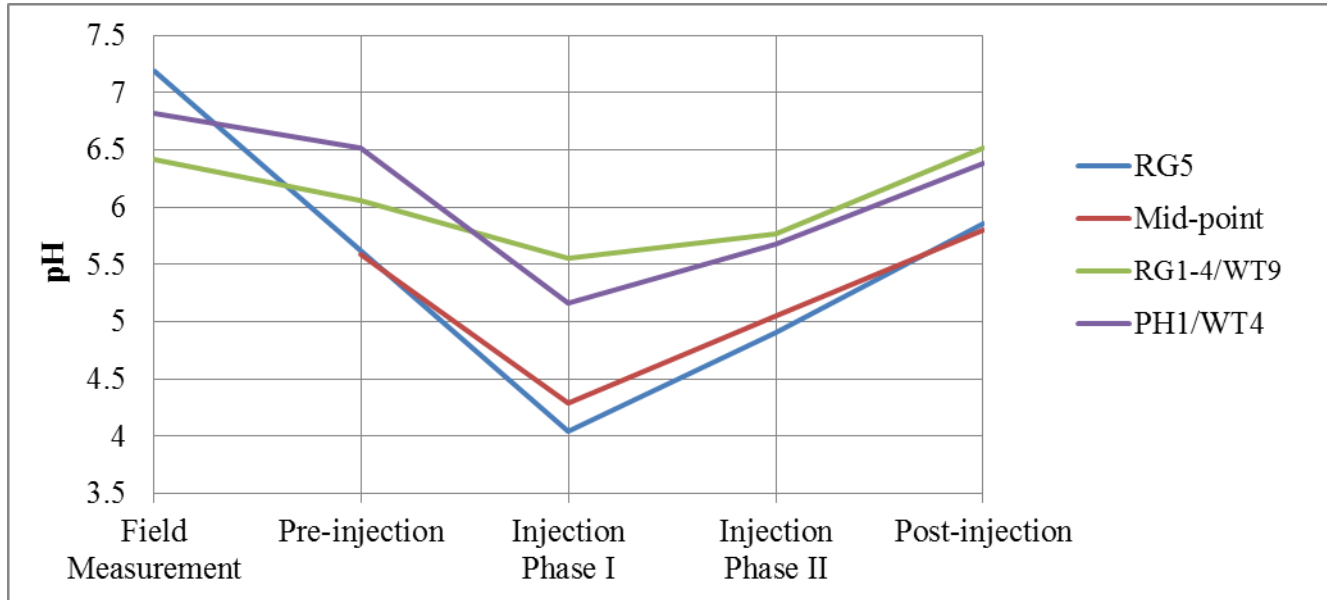


Figure 5.1 pH versus GWB simulation phase for the Jackson reservoir rocks. The pH response within the seal rocks (not shown) follows an identical pattern to the pH change within the reservoir rocks for the first two simulation phases. For the final two phases, the pH in the seal rocks is slightly less than in the reservoir rocks at each of the well locations (Tables 5.1a, 5.1b).

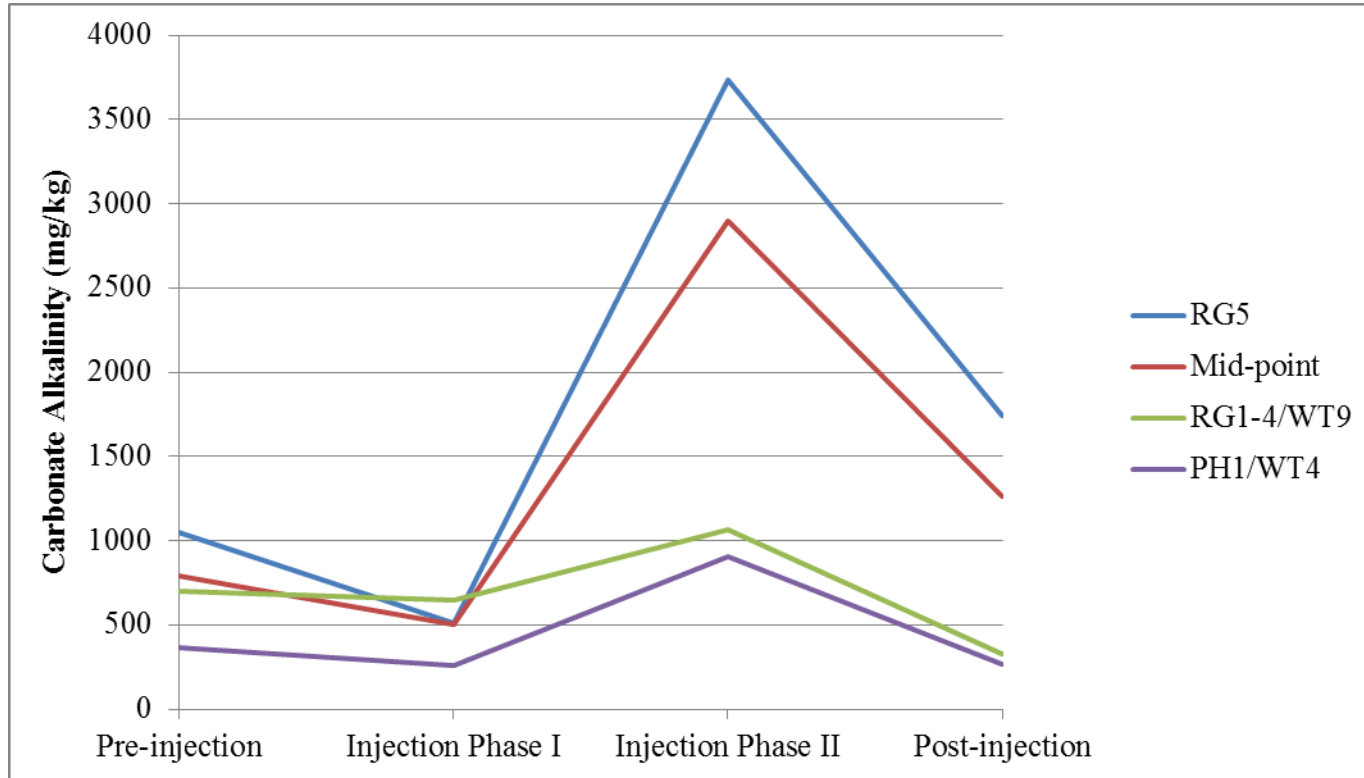


Figure 5.2 Carbonate alkalinity (mg/kg) versus GWB simulation phase for the Jackson reservoir rocks. The carbonate alkalinity response within the seal rocks (not shown) follows an identical pattern to the change within the reservoir rocks for the first two simulation phases. For the final two phases, the carbonate alkalinity in the seal rocks is less than in the reservoir rocks at each of the well locations (Tables 5.1a, 5.1b).

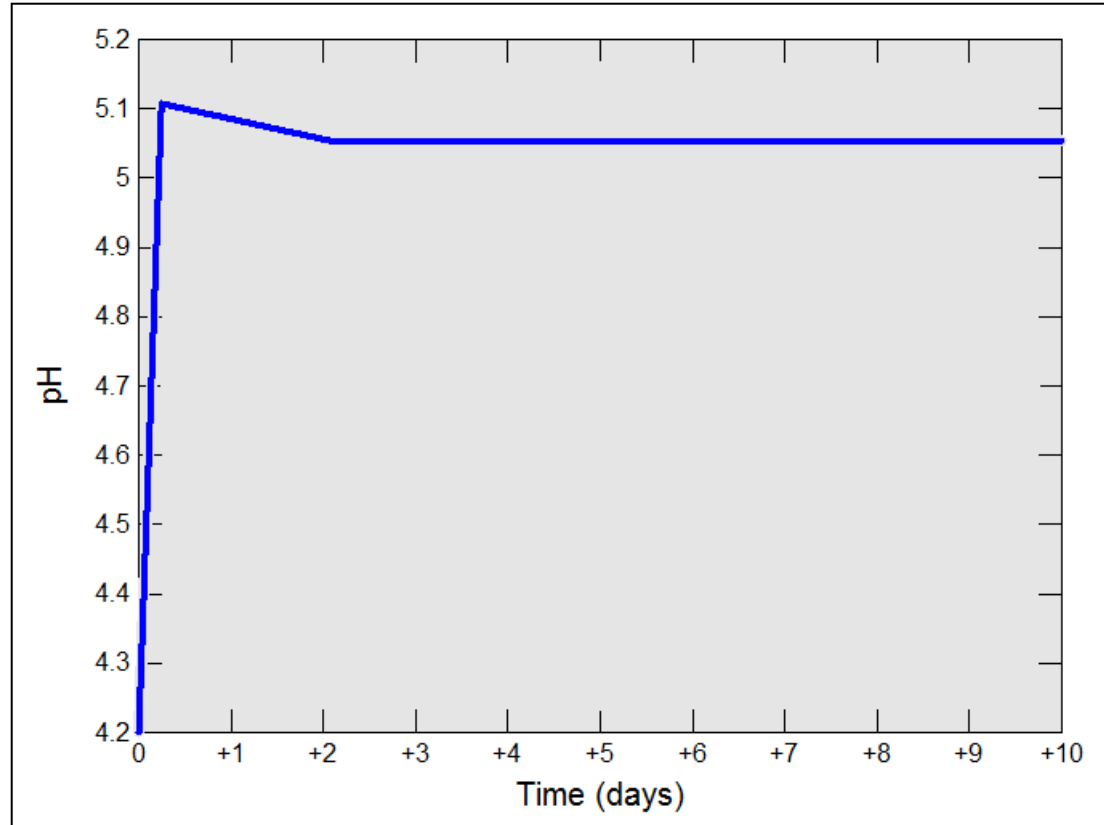


Figure 5.3 pH versus time for mid-fugacity during the CO₂ injection phase II when kinetic minerals were titrated into the system. The model predicts a very rapid pH increase and a similar plot for carbonate alkalinity as well.

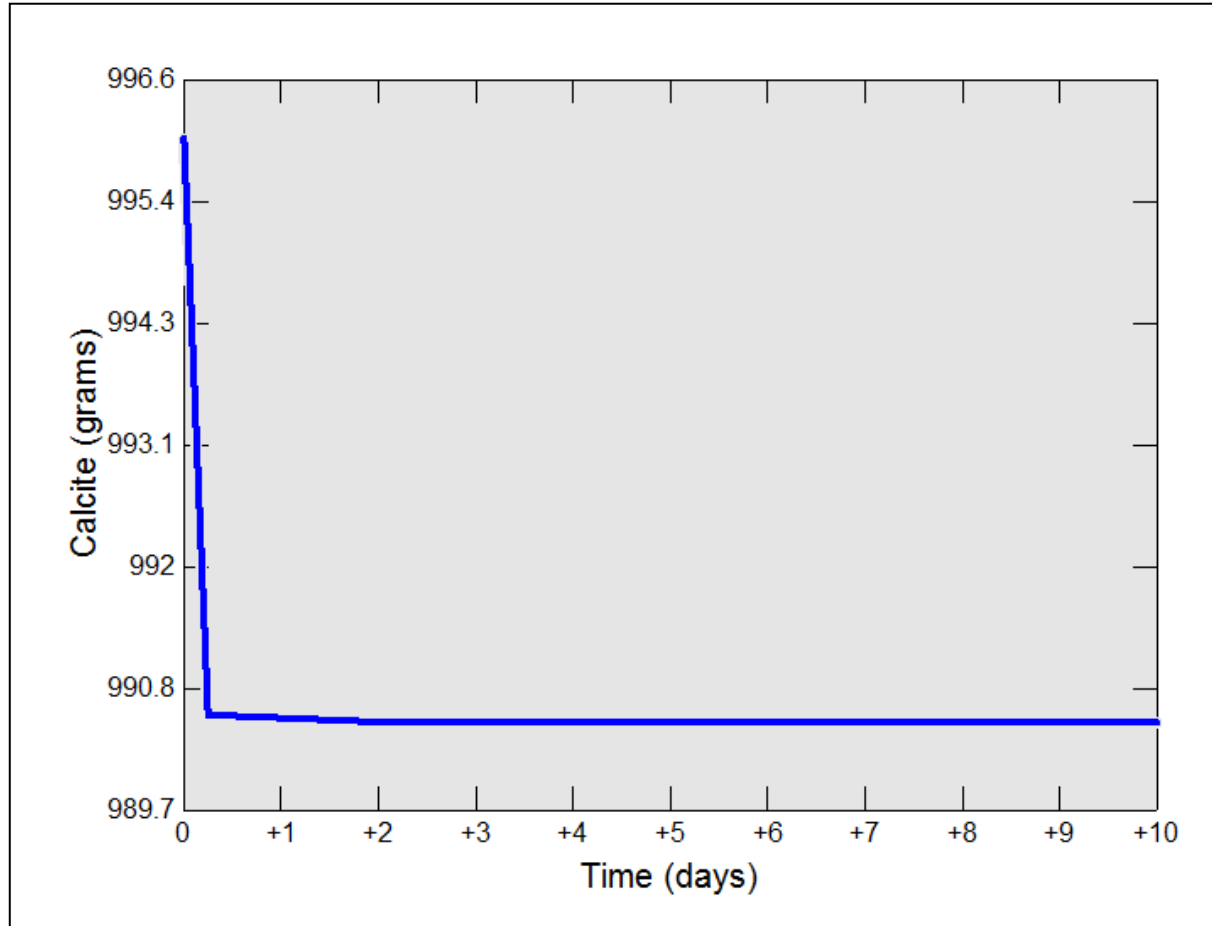


Figure 5.4 Mass of calcite versus time for the mid-fugacity showing the rapid calcite dissolution during the CO₂ injection phase II when kinetic minerals were titrated into the system. The model predicts the dissolution of approximately 5.5 grams of calcite.

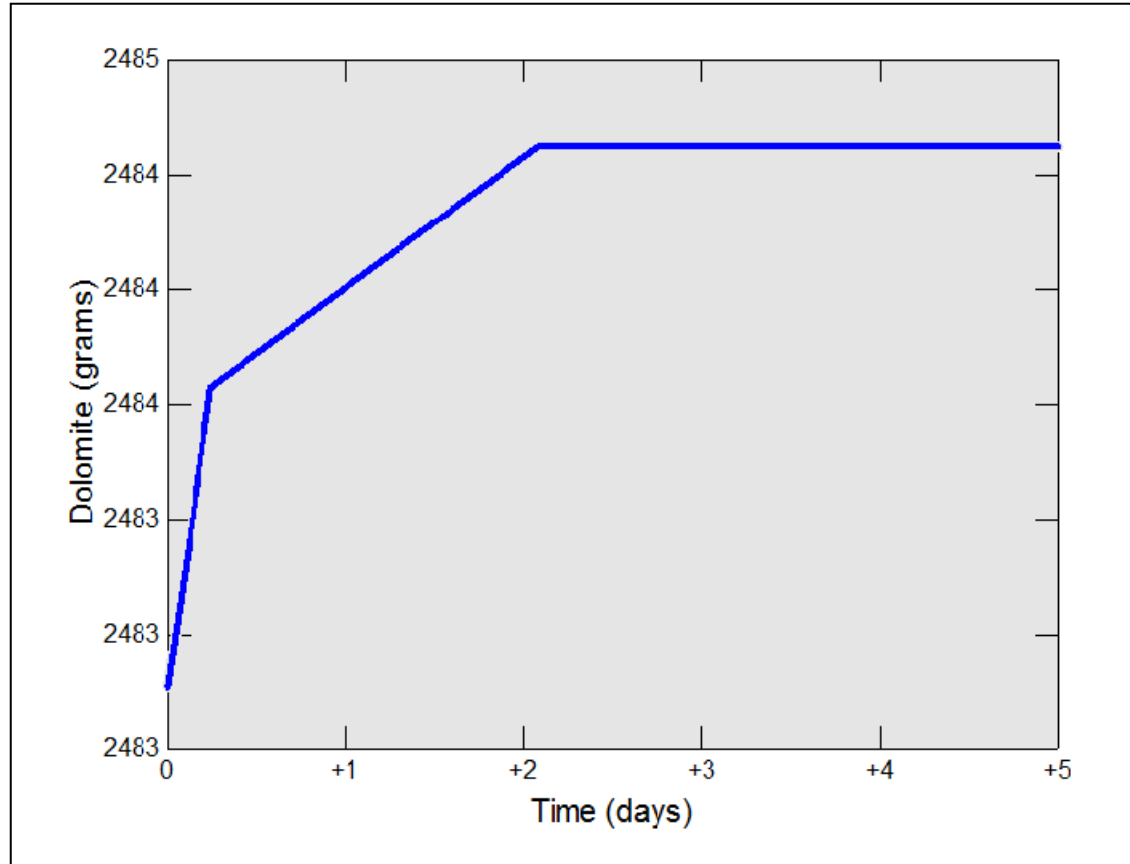


Figure 5.5 Mass of dolomite versus time at the mid-fugacity showing the rapid precipitation of dolomite during CO₂ injection phase II when kinetic minerals were titrated into the system. The model predicts the precipitation of approximately 1.4 grams of dolomite.

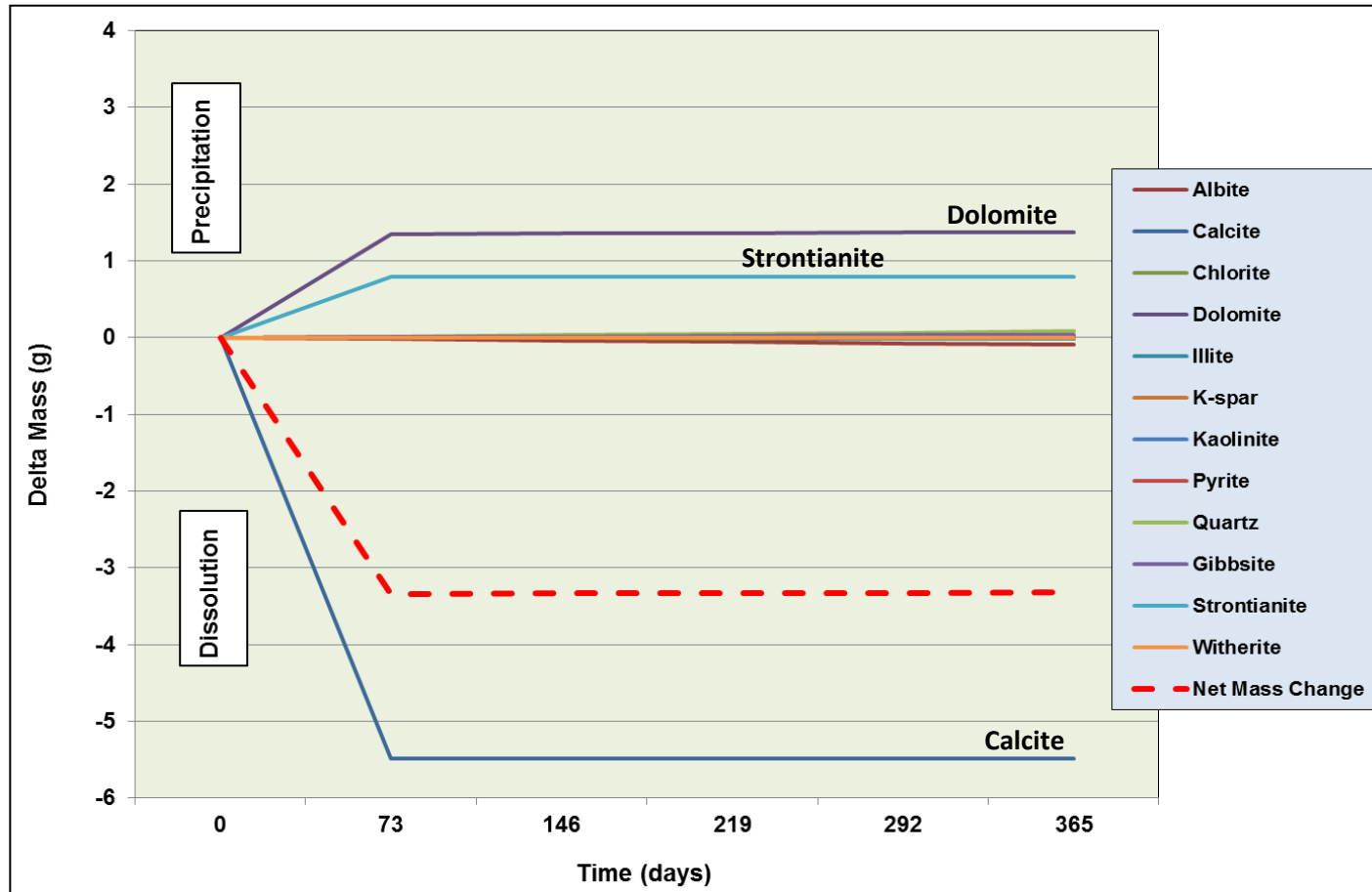


Figure 5.6 Change in mass (delta mass) versus time in days for reservoir rocks at the mid-point fugacity during CO₂ injection phase II. The model shows dissolution of calcite and precipitation of dolomite-ankerite and strontianite. The magnitude and rates of mass change associated with carbonates far exceeds those for alumino-silicate minerals (lines with low gradient slopes near the zero delta mass axis). The magnitude of calcite dissolution exceeds precipitation for all carbonate and alumino-silicate minerals leading to net dissolution. Mass changes for other simulation scenarios follow a similar pattern (Tables 5.3a, b).

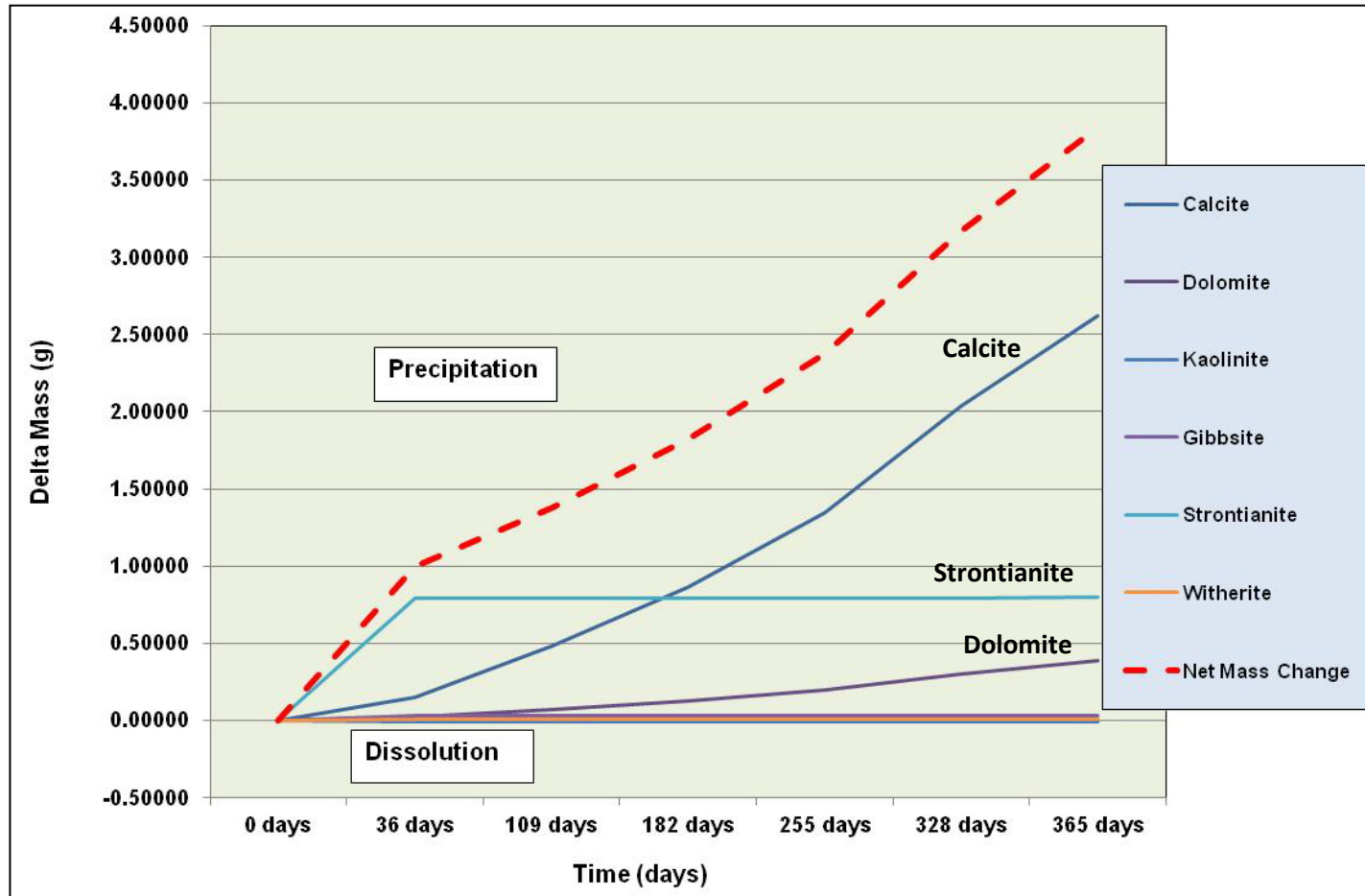


Figure 5.7 Example of change in mass (delta mass) versus time for reservoir rocks at the mid-point fugacity during the post-CO₂ injection phase. The model shows net precipitation as controlled by precipitation of calcite, dolomite and strontianite. As in Figure 5.6, the magnitude and rates of mass change associated with carbonates far exceeds those for aluminosilicate minerals (lines with low gradient slopes near the zero delta mass axis). Mass changes for other simulation scenarios follow a similar pattern (Tables 5.3a, b).

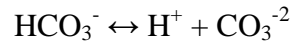
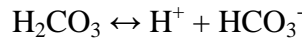
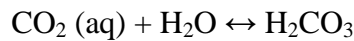
Chapter 6: GWB Modeling Discussion

The simulations completed in this study were conducted under conditions of constant temperature and constant starting mineralogy for the reservoir and seal rocks at each of the four well locations. Therefore, the main variable that influences the types and magnitudes of geochemical subsurface interactions is the variation of $f\text{CO}_2$ to simulate the phases of CO_2 injection. An additional variable that influences geochemical reactions within this study is the variation in formation water chemistry among the wells before CO_2 injection occurred. An examination of how these variables affects water chemistry, mineral saturation, mineral reactions, and porosity is discussed in this section.

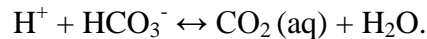
As previously noted, water injection of the more dilute, NaHCO_3 -rich, Pennsylvanian water from WT3 into the reservoir during the water flood results in formation water that is more dilute at RG5, RG1-4, WT9 as compared to PH1, WT4, which are unaffected by the flood (Table 4.1a, Figure 4.3). The PH1, WT4 wells are used as representative of pristine Jackson formation water, and the results provide insight into possible reactions in a Mississippian oil reservoir that was not previously water flooded. This difference in pre- CO_2 aqueous chemistry among the wells affects several variables and is the justification for having distinct simulations for two sets of production wells within the reservoir and seal rocks. For example, the injected NaHCO_3 -rich Pennsylvanian water explains why higher alkalinities are associated with RG5 and RG1-4, WT9. Additionally, the formation waters from PH1, WT4 have over double the amount of calcium and magnesium as compared to RG1-4, WT9. The elevated amount of carbonate mineral-forming ions in solution at PH1, WT4 indicates a greater potential buffering capacity during CO_2 injection, which will be discussed later on. The dilution of

the Jackson formation water also produces greater degrees of undersaturation, especially for alumino-silicate minerals and carbonates, at RG5, while alumino-silicates and carbonates are slightly saturated and super-saturated at RG1-4, WT9 and PH1, WT4, respectively. Pyrite is super-saturated at all well locations, especially PH1, WT4, likely as a direct result of an anomalously high iron concentration before CO₂ was injected.

For the CO₂ injection phase I simulation it is important to discuss the relationship between pH and changes in *f*CO₂. Recall that in order to simulate CO₂ injection, *f*CO₂ is increased, which can be described using following dissociation reaction that produces H⁺ ions:

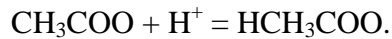


The pH is a measure of the H⁺ ions in the formation water, so by increasing *f*CO₂ and aqueous CO₂ during injection phase I, the pH decreases. The rate of pH decrease is rapid early on, and the rate declines with successively higher *f*CO₂ and aqueous CO₂ values (Figure 5.1). The more gradual pH decrease as *f*CO₂ increases likely reflects the reaction of H⁺ ions and HCO₃⁻ to produce H₂O and CO₂ (aq):

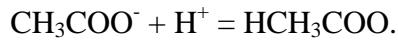


When pH versus reaction progress is examined for each well simulation, none show any significant slope breaks that could be attributed to significant buffering reactions during injection phase I because there are no kinetic minerals included in the system yet. The decrease in alkalinity during injection phase I probably reflects the

consumption of the aqueous HCO_3^- species (the predominant carbonate species at lower pH) due to the previously described reaction with H^+ to form aqueous CO_2 and H_2O . In addition, the concentrations of acetate (CH_3COO^-), which also contributes to alkalinity, are reduced as acetic acid (HCH_3COO) forms:



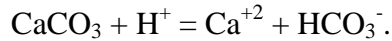
The decrease in alkalinity during injection phase I probably reflects the reaction of HCO_3^- (the predominant carbonate species at lower pH) with H^+ to form $\text{CO}_2(\text{aq})$ and H_2O . In addition, CO_3^{2-} and CH_3COO^- (acetate) were also consumed (Figure 6.1) in buffering reactions, with the latter demonstrated by:



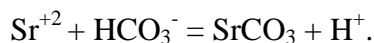
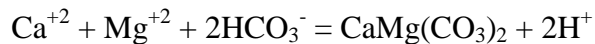
Over the simulated pH range, the concentration of aqueous HCO_3^- species was typically one- to two-orders of magnitude greater than CO_3^{2-} and two- to four-orders greater than CH_3COO^- . The previously described pattern of decreased CO_3^{2-} , HCO_3^- and CH_3COO^- (hence decreased alkalinity), and increased $\text{CO}_2(\text{aq})$ and HCH_3COO is similar among all the well simulations with increased $f\text{CO}_2$. The effects of the varying pre- CO_2 injection formation water chemistries are evidenced during injection phase I as well. For example, when $f\text{CO}_2$ is increased to 1.68 bars at the production wells, the result was a greater pH decrease at PH1, WT4 versus RG1-4, WT9 (Tables 5.1a, b). The greater decrease in pH is almost certainly due to the lower alkalinity (and decreased ability to buffer pH) before CO_2 injection at PH1, WT4.

As the kinetic minerals are titrated in and $f\text{CO}_2$ is held constant for the yearlong CO_2 injection phase II, a more effective buffering system is observed and thus represents a more realistic depiction of the aggregate formation water and mineral system. Increases

in pH and carbonate alkalinity at all wells in association with mineral titration underscored the importance of mineral reactions in buffering the formation water in both the reservoir and seal rocks. Analysis of mass changes (Tables 5.3a-d) show that calcite dissolution occurs within day of mineral titration (Figure 5.4) and is largely responsible for buffering, according to the reaction:



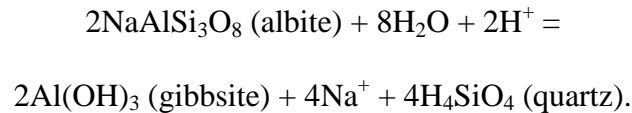
It is likely that the calcite dissolution also drives the precipitation of both dolomite (Figure 5.5) and strontianite in all the wells. The precipitation of carbonate minerals indicates mineral trapping of CO₂, but the mass of calcite dissolving is greater and causes a net dissolution (Figure 5.6) in the reservoir and seal rocks for all of the well simulations. This suggests that precipitation of these carbonates, despite low pH, is driven by increases in Ca⁺² and HCO₃⁻ to varying degrees at all wells, again as a result of differences in formation water chemistry from pre-CO₂ injection. General reactions for precipitation of dolomite and strontianite, respectively, are:



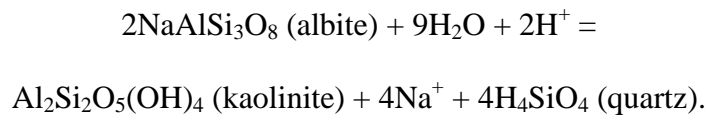
It is important to note, however, that ankerite (CaFe(CO₃)₂) makes up a significant portion of the carbonate mass in many of the reservoir and seal rock samples. Despite this, ankerite is not included as a mineral in the simulation because thermodynamic data for equilibrium values and kinetic data for reaction rates are lacking for GWB. Consequently, dolomite, which actually represents a smaller part of the carbonate fraction, is used as a proxy for ankerite. Justification for doing this is because ankerite is isostructural with dolomite and the two minerals form a complete solid solution series

(Nesse, 2000). Therefore, it is possible that ankerite precipitation might occur in addition to dolomite for the well simulations during injection phase II in the reservoir and seal rocks.

Analysis of the saturation indices indicate that the formation water is undersaturated with respect to illite, K-feldspar, and albite at the beginning of CO₂ injection phase II at all of the wells in both the reservoir and seal rocks. The undersaturation results in the dissolution of these minerals over the yearlong kinetic mineral titration period. The mass changes (Tables 5.3a-d) show that most dissolution is associated with albite and smaller amounts of K-feldspar, illite, and chlorite (Figure 6.2). The amount of precipitated quartz and gibbsite suggests that these are largely reaction products from albite dissolution in accordance with the general reaction:



If albite were the only alumino-silicate mineral affected by dissolution, then the mass units dissolved and precipitated could be estimated using the slope-of-line methods in GWB (Bethke, 2008). This is not the case, however, as dissolution of K-feldspar, illite, and chlorite potentially produce some of the same reaction products. Thus, the analysis is restricted to general reactions only, for example:



Despite the number of possible reactions, the overall mass involved in the alumino-silicate reactions is so small (less than 1 gram), due to slow reaction rates (White and Brantley, 1995; Brantley, 2008). Consequently, the formation water in the reservoir and

seal rocks remains undersaturated with respect to the alumino-silicates at the end of CO₂ injection phase II (Tables 5.2a-d).

Recall that the post-CO₂ injection phase at Sugar Creek represents a sliding $f\text{CO}_2$ model in which $f\text{CO}_2$ is reduced back down to pre-CO₂ injection values. Decreasing the $f\text{CO}_2$ causes the pH to increase at all the well locations for both the reservoir and seal rocks, although at differing magnitudes due to the spatial $f\text{CO}_2$ variation and starting formation water chemistry variation among the wells. Analysis of aqueous carbon species for this phase shows that most alkalinity is accounted for by HCO₃⁻ species. Mass changes for all the well simulations in the reservoir and seal rocks (Tables 5.3a-d) show that the decreased alkalinity can largely be attributed to the removal of HCO₃⁻ through precipitation of calcite, strontianite, and dolomite (ankerite). Further examination, however, shows no mass changes for most of the alumino-silicate minerals. The reason for this absence represents a limitation of the post-CO₂ injection phase, in which minerals could not be included as reactants. To circumvent this issue, the carbonate minerals are substituted into the basis (e.g. calcite for Ca⁺²), while the alumino-silicate minerals not in equilibrium with the formation water at the end of CO₂ injection were not substituted into the basis. As discussed in the analysis of mineral precipitation for CO₂-injection phase II, the alumino-silicate reactions might not be important from a mass perspective, but some dissolution of feldspars, illite, and chlorite would likely continue in the post-CO₂ injection phase since they remain undersaturated at all of the wells. Modeling with a sliding-fugacity model without explicitly addressing the alumino-silicate interactions therefore does not provide a complete representation of mass changes in the post-CO₂ injection phase. Though mass changes through dissolution or precipitation of alumino-

silicates might be small, they might have significant effects, especially in the seal rock where porosity is low.

The overall analysis of GWB model predictions for each of the four phases shows numerous similarities between the seal and reservoir rocks. Changes observed in reservoir rocks are mimicked by seal rocks; however, the magnitude of each change is not necessarily equal due to the different starting mineral assemblages. Similarly, changes observed at the injection well, mid-fugacity, and production wells (RG1-4, WT9 and PH1, WT4) all follow a similar pattern, although at different magnitudes as a direct result of the water flood effects on starting formation water chemistry. It should be noted that the GWB model initially predicts the following suite of minerals to precipitate throughout each of the four simulations: dawsonite, dolomite-ord, and dolomite-dis. On a geologic basis, however, a determination was made that they are all unlikely to precipitate under these reservoir conditions within such a short injection time scale. Consequently, they have been suppressed within the system and not allowed to precipitate at all. Several other minerals, including alunite and graphite, are also predicted to precipitate during the modeling process but have been ignored due to the unlikelihood of their occurrence within the reservoir conditions.

6.1 Porosity Effects

Because carbonate reactions account for the greatest changes in mass and volume within the reservoir and seal rocks at the well locations, they also have the greatest influence on porosity. To determine the effects of these geochemical reactions have on porosity, the total change in porosity must be determined. To do that, the total change in

mineral volume is divided by the total volume of the reservoir and seal, respectively. Using the mass change results from the final two phases (CO₂ injection phase II and post-CO₂ injection phase) gives a change in porosity of less than one percent in both the reservoir and seal rocks (Table 6.1). There is a net dissolution and net precipitation within the reservoir rocks during CO₂ injection phase II and post-CO₂ injection phase, respectively. This means that porosity is created during mineral titration whereas the minerals precipitating in the final phase of simulation causes porosity to decrease. In the seal rocks there is a decrease in porosity for both of the aforementioned phases. However, such a minimal change would have negligible effects on both seal integrity and ability to prevent the upward migration of CO₂.

6.2 Model Predictions versus Field Measurements

The monitoring program before, during, and after CO₂ injection pilot project at Sugar Creek allows the opportunity for a comparison between GWB predictions and actual field data. The discrepancy between the measured pH values and the model's pH predictions during the pre-CO₂ injection phase likely represents field error. Although all precautions were taken to avoid contact between the atmosphere and the sampled formation water, sample degassing was unavoidable. Pressure decreased as the sample was brought from the reservoir to the surface, and as a result the concentration of CO₂ (and acidity of the water) decreased. Therefore, the model's prediction for starting pH of the formation water (e.g. 5.62 at RG5) with a concentration of 3.5% CO₂ might be a closer representation than the measured value from the field (e.g. 7.19 at RG5).

During CO₂ injection, the pH decrease (approximately 1 pH unit) occurred very close to the time of CO₂ breakthrough at wells affected by the water flood. One limitation of injection phase II is that the kinetic minerals are titrated into CO₂-rich, low-pH formation water so that reactions start immediately. This results, for example, in the carbonates reacting within days of the mineral titration. The field measurements do reveal a rapid increase in concentrations of Ca⁺², Mg⁺², Sr⁺² and Fe⁺², which suggests carbonate dissolution and solubility trapping within the reservoir. However, the dissolution occurs within weeks and months as opposed to instantaneously (Frailey *et al.*, 2012). Therefore, the GWB model for injection phase II likely overestimates the degree of geochemical interactions within the reservoir and seal rocks.

After CO₂ injection ceased, the Jackson formation water had persistently low pH values (5.7-6.2) and elevated alkalinity over the yearlong monitoring program (Frailey *et al.*, 2012). As with the GWB model, field results indicate minimal, if any, mineral trapping within the reservoir and solubility trapping as the main mechanism for sequestration of CO₂. Overall, the model is generally successful in predicting the types of reactions occurring before, during, and after CO₂ injection at Sugar Creek; however, aqueous geochemical responses are slower in real time, as evidenced by actual field data as compared to model simulations.

Table 6.1 Calculated change in porosities after CO₂ injection phase II and post-CO₂ injection phase for Jackson reservoir and seal rocks. Positive values indicate a net dissolution (porosity increase) whereas negative values indicate a net precipitation (porosity decrease).

	CO ₂ injection phase II	Post-CO ₂ injection phase
Reservoir Rocks	0.0078%	-0.0078%
Seal Rocks	-0.00057%	-0.0045%

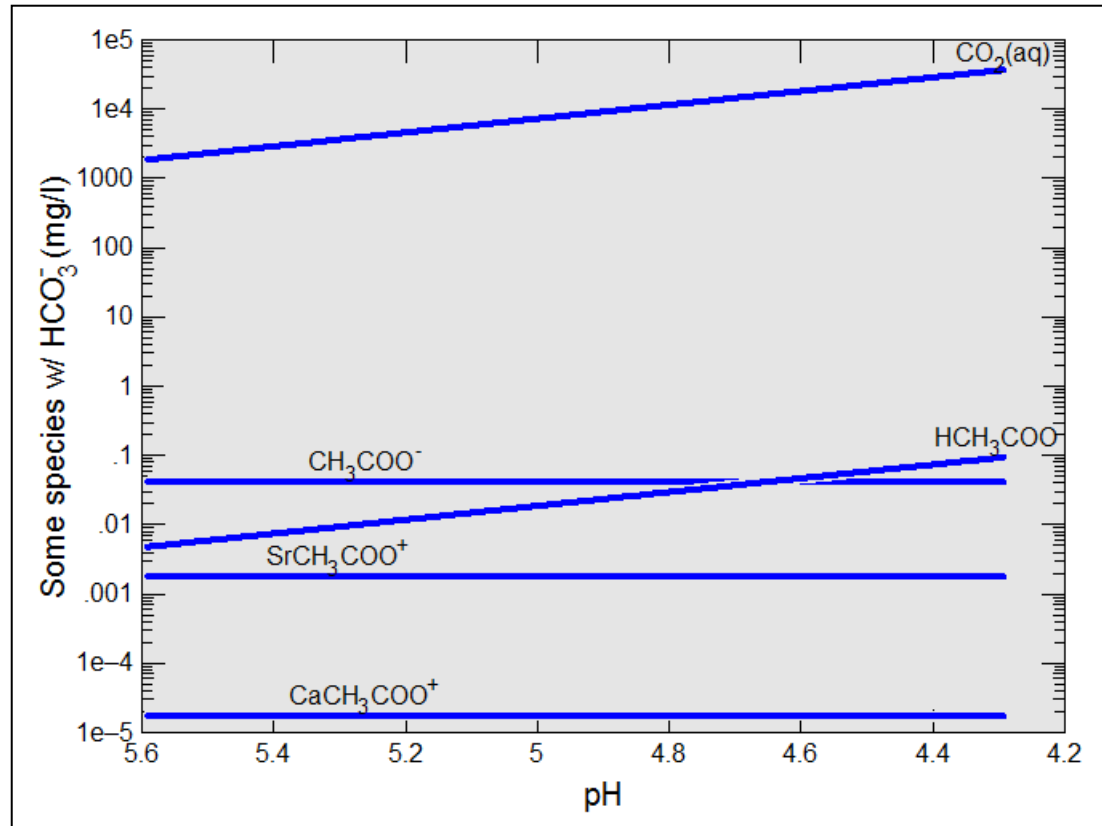


Figure 6.1 Plot from GWB showing HCO_3^- species interactions as pH rapidly decreases during CO_2 injection phase I. Acetate (CH_3COO^-) combines with hydrogen ions (H^+) to form acetic acid (HCH_3COO).

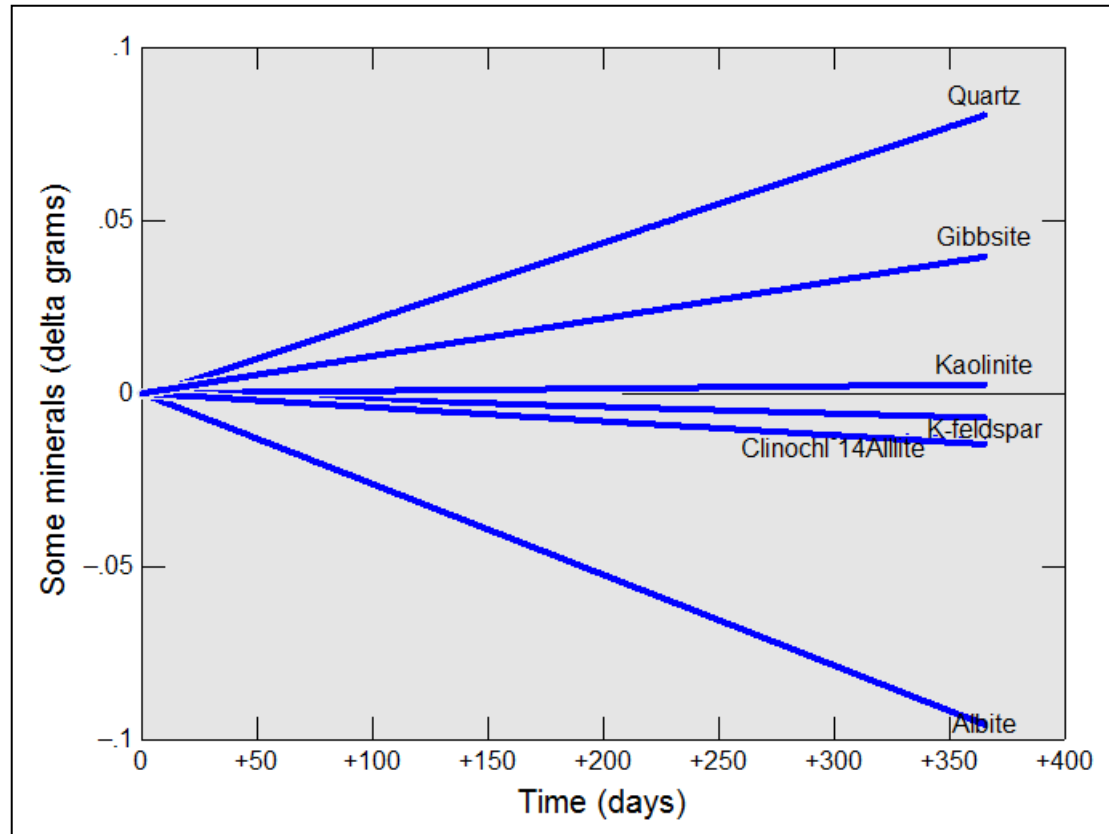


Figure 6.2 Plot from GWB showing delta mass (grams) versus time in days for some alumino-silicate minerals during CO₂ injection phase II for the mid-point fugacity. Chlorite is represented as chlinochlor-14A in the plot.

Chapter 7: Conclusions

Geochemical modeling of CO₂ injection in the Mississippian Jackson sandstone (Jackson) reservoir at Sugar Creek oil field provides insight into geochemical interactions among CO₂, rock-forming minerals, and formation water in the reservoir and seal. Inputs for the GWB model include a robust set of water chemistry data attained from formation water samples collected in and around Sugar Creek field, as well as reservoir and seal mineralogy data collected from XRD analysis of cuttings samples. This study also provides the opportunity to compare modeling results with actual geochemical measurements collected at Sugar Creek as part of a CO₂ injection pilot program administered by the Midwest Geological Sequestration Consortium. CO₂ fugacity ($f\text{CO}_2$), a critical variable in this study, is calculated from pressure and gas composition data collected in the field before, during, and after CO₂ injection (Frailey *et al.*, 2012).

Analysis of formation water in the Jackson reservoir and seal indicates NaCl-rich water, but with a wide range of salinity values. The variation in salinity is likely due to variations in the degree of mixing between original Jackson formation water and fresher water taken from an overlying Pennsylvanian aquifer and used for secondary recovery. The variation in salinity distribution in the field indicates compartmentalization of the Jackson reservoir. XRD analysis coupled with macroscopic examination shows Jackson reservoir samples to be primarily quartz-rich sandstones cemented with quartz, calcite, dolomite, and ankerite. The overlying seal rocks in the upper Jackson and Golconda Formation show a decreased quartz content and increased weight percent of clay, feldspar, and carbonate. The Jackson mineral assemblage is similar to other Chesterian sandstone formations such as the Tar Springs and Hardinsburg (Swann, 1967). Therefore,

the predicted reactions associated with CO₂ injection would likely be similar among the Chesterian sandstone reservoirs. The potential application of CO₂ storage and CO₂-enhanced oil recovery in other Chesterian reservoirs in the southern Illinois basin is further supported by similar temperatures and pressures among them (Takacs *et al.*, 2010; Frailey *et al.*, 2012).

Modeling is accomplished by using four phases: 1) pre-CO₂ injection, 2) CO₂ injection phase I, 3) CO₂ injection phase II, and 4) post-CO₂ injection. During and after CO₂ injection, a variety of reactions are capable of geochemically trapping CO₂ in the Jackson sandstone reservoir. During CO₂ injection, pH values decreased 0.3 to 0.9 pH units, suggesting the dissolution of CO₂ into formation water and subsequent dissociation of carbonic acid. Simulations representing continuous CO₂ injection over one year suggest that dissolution of calcite will be the dominant reaction influencing the change of mass within the reservoir and seal rocks. Dissolution thus predicts that CO₂ will be trapped in solution (solubility trapping). Despite decreases in pH to values ranging from 4.9 to 5.7, calcite dissolution provides Ca⁺² and HCO₃⁻ that drives precipitation of dolomite (ankerite) and strontianite. The precipitation of the carbonate minerals thus represents the potential for mineral trapping even as CO₂ is being injected. Analysis of alumino-silicate mass changes shows that most dissolution is associated with albite and smaller amounts of K-feldspar, illite, and chlorite. The overall mass change involved in the alumino-silicate reactions is much smaller than carbonates, which can be attributed to slow reaction rates (White and Brantley, 1995; Brantley, 2008). However, the alumino-silicate reactions might still have significant effects, especially in the seal rock where porosity is low.

The potential for mineral trapping continues into the post-CO₂ period as the calcite and smaller amounts of dolomite (ankerite) and strontianite are predicted to precipitate in the reservoir rocks. The increased alkalinity and cations (i.e. Ca⁺², Sr⁺², Mg⁺²) provided by the dissolution of carbonates during the CO₂ injection simulation steps allows calcite, dolomite, and strontianite to precipitate in the post-CO₂ simulation, where *f*CO₂ is returned to pre-CO₂ injection values. The alumino-silicate minerals, such as K-feldspar, albite, chlorite, and illite are undersaturated at the end of the CO₂ injection simulation steps and therefore are not explicitly included in the basis or as reactants in the post-CO₂ simulation. Consequently, the reaction paths of these minerals are not modeled; however, it is likely that they would continue to dissolve albeit at declining rates as pH increased to pre-CO₂ injection values. The top three minerals (based on volume precipitated) post-CO₂ injection in the seal rocks are calcite, dolomite (ankerite), and kaolinite (Al₂Si₂O₅(OH)₄). As with reservoir rocks, the Ca⁺² and Mg⁺² needed for calcite and dolomite precipitation are already present in the initial system, and K-feldspar dissolution contributes Al to the system in order to produce kaolinite.

Despite accounting for most of the mass and volume change during CO₂ injection, the carbonate reactions caused porosity to increase and decrease by less than one percent in the reservoir and seal rocks, respectively. After CO₂ injection, the carbonate precipitation reactions caused porosity to decrease by less than one percent in both the reservoir and seal rocks. Although simulated porosity changes were negligible for this study, field projects with longer injection intervals will likely see more significant changes as the CO₂-water-rock reactions in the reservoir and seal intervals will occur

over longer periods of time. Precipitation of carbonate in the seal rocks would further reduce porosity and enhance seal properties.

The post-CO₂ injection phase, in which a sliding $f\text{CO}_2$ model is used, is likely the least effective of the simulation steps in accurately representing the geochemical evolution in the reservoir. The full suite of potential geochemical interactions is not addressed as most of the alumino-silicate minerals are not included. Moreover, the post-CO₂ period at Sugar Creek represents a return to water flood. Geochemically, this is significant, because the injection water mixture includes NaHCO₃-rich water that could react with alkaline earth cations (e.g. Ca⁺², Sr⁺², Mg⁺²) whose values are elevated because of mineral dissolution during CO₂ injection. Because of this, the sliding fugacity model likely underestimates potential mineral trapping. Using GWB's mixing model function would provide a more accurate estimate of geochemical interactions in the post-CO₂ phase.

7.1 Limitations of Geochemical Modeling

Geochemical modeling is a powerful tool that can allow for the analysis of long-term reactions not able to be readily studied within a laboratory. Nevertheless, it is important to note that the model created is only as accurate as the input data provided and the overall understanding of a given system. Although this study provides high quality data from a pilot project and successfully notes important subsurface reactions, additional detailed work is needed. As noted in the previous section, one major limitation to the modeling conducted in this study is that there is no reactive transport component, which integrates geochemical and hydrological processes in complex geologic systems. The

modeling results from this study allow for general statements to be made regarding potential reactions occurring, but they do not explicitly address the distribution of free-phase CO₂, how spatial variations in reservoir properties might influence the timing of geochemical reactions, and how those reactions could affect reservoir properties. Therefore, a more in-depth estimate of the fate of CO₂ should include a transport component. Additionally, the modeling should address transport and reactions where multiple fluid phases are present, such as CO₂, oil, and formation water. Another limitation in the study includes the GWB software itself, which was not designed to simulate reactions under high CO₂ fugacity. The GWB database had to be updated to account for the salting-out effect and other alterations (i.e. kinetic reaction rates) were made in order to allow the system to come to equilibrium (Allen *et al.*, 2005).

7.2 Future Work

Future geochemical reaction studies involving CO₂ injection would benefit by comparing the fate of CO₂ in reservoirs where CO₂ is miscible versus immiscible. In the Illinois basin, the targeted potential EOR resource includes immiscible and miscible oil fields (U.S. DOE, 2012). Successful analysis would require the ability to model reactions with multiple phases. Lastly, although most oil occurs in clastic reservoirs in the Illinois basin, it would be beneficial to compare the differences in geochemical interactions between clastic and carbonate reservoirs, the latter of which are important in other parts of Kentucky.

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Vita

Anne Schumacher

Born in Kalamazoo, MI

Prior Education

- Bachelor of Arts, Geology from Albion College, Albion, MI

Prior Experience

- Geologist, Rhino Resource Partners LP (Lexington, KY)
- Student Researcher, Kentucky Geological Survey (Lexington, KY)
- Teaching Assistant, Department of Earth and Environmental Sciences, University of Kentucky (Lexington, KY)
- Field Hydrogeologist, Bureau of Land Management (Durango, CO)

Professional Memberships

- Geological Society of America
- American Association of Petroleum Geologists
- National Groundwater Association

Professional Publications and Presentations

- **Schumacher, A.M.**, T. M. Parris, A. E. Fryar, E. G. Beck, and K. G. Takacs. (2010) Modeling of CO₂-water-rock interactions in Mississippian sandstone reservoirs of Kentucky. AAPG Eastern Section Meeting, Kalamazoo, MI.
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