



**José Miguel Botica Rodrigues**

Licenciatura em Engenharia de Materiais

## **Production and characterization of magnetic bioactive glass membranes**

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Orientador: Professor Doutor João Paulo Miranda Ribeiro Borges, Professor Associado com agregação, Faculdade de Ciências e Tecnologia da Universidade Nova de Lisboa

Co-orientadora: Doutora Paula Isabel Pereira Soares, Investigadora em Pós-Doutoramento, Faculdade de Ciências e Tecnologia da Universidade Nova de Lisboa



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## Resumo

O tratamento do cancro do osso geralmente origina defeitos ósseos com células tumorais residuais que proliferam durante a regeneração óssea. Portanto, é necessária uma estrutura para a regeneração óssea que simultaneamente mate células tumorais residuais. Este projeto visa produzir um sistema composto por um vidro bioativo (BAG) e nanopartículas magnéticas (MNPs). Este sistema é altamente bioativo e reabsorvível devido ao vidro bioativo que leva à formação da camada de hidroxiapatite (HA) que faz uma ligação entre o material e o osso. As nanopartículas magnéticas atuam como sementes gerando calor clinicamente relevante, sob aplicação de um campo magnético alternado, para matar ou sensibilizar células tumorais. Em combinação com a liberação de um fármaco citotóxico, este sistema compósito efetivamente irá matar as células do tumor ósseo enquanto fornece a base para a regeneração óssea.

O BAG foi produzido por uma técnica simples de sol-gel assistida por EISA (*Evaporation induced self-assembly*). Um moinho de bolas foi utilizado para diminuir o tamanho das partículas do BAG e aumentar sua dispersabilidade. Os pós foram caracterizados por SEM (microscopia eletrônica de varrimento), EDS (espectroscopia de dispersão de energia por raios X), e FTIR (Espectroscopia por Infravermelho com Transformada de Fourier). As IONPs foram produzidas por co-precipitação química e revestidas com ácido oleico para evitar a agregação e a perda de propriedades superparamagnéticas com o tempo. As membranas de PVP/BAG foram produzidas por eletrofição e os parâmetros foram otimizados de modo a produzir fibras de diâmetros menores, uma vez que isto se traduz numa maior área de superfície e maior bioatividade. Os IONPs foram então incorporados na solução por agitação mecânica.

As membranas eletrofiadas foram reticuladas devido à solubilidade do PVP em água. Para tal foi utilizada a reticulação por UV e térmica, mas apenas a reticulação térmica provou ser bem-sucedida. Neste aspeto, a análise TGA/DSC foi importante para encontrar a temperatura de reticulação do PVP e forneceu algumas informações sobre a estabilidade térmica das membranas.

As membranas compósitas insolúveis em água foram testadas para aplicação em hipertermia magnética e a sua citotoxicidade foi também avaliada. As IONPs provaram ter propriedades superparamagnéticas e uma pequena variação de temperatura foi alcançada para uma amostra de 10 mg de membrana, demonstrando o potencial das membranas compósitas para esta aplicação.

**Palavras-chave:** Hipertermia magnética, membranas compósitas, nanopartículas de óxido de ferro, regeneração óssea, vidro bioactivo.





## Abstract

Bone cancer treatment usually originates bone defects with residual tumour cells that can proliferate during bone regeneration. Therefore, a scaffold for bone regeneration that simultaneously kill residual tumour cells is needed. This project aims at producing a composite system composed of a bioactive glass (BAG) and magnetic nanoparticles (MNPs). This system is highly bioactive and reabsorbable due to the bioactive glass which leads to formation of a hydroxyapatite (HA) layer that bonds to bone. The system is biodegradable at an adequate rate for bone regeneration. Magnetic nanoparticles act as thermoseeds generating clinically relevant heat under an applied alternating magnetic field to kill or sensitize tumour cells. In combination with release of an anticancer drug, this composite system will effectively kill bone tumour cells whilst providing a base for bone regeneration.

BAG was produced by a simple sol-gel technique assisted by EISA (Evaporation Induced Self-Assembly). Ball milling equipment was used to decrease the BAG particle size and increase its dispersibility. The powders were characterized by SEM (scanning electron microscopy), EDS (energy dispersive x-ray spectroscopy), and FTIR (Fourier Transform Infrared Spectroscopy). IONPs were produced through chemical co-precipitation and coated with oleic acid to avoid aggregation and loss of superparamagnetic properties over time. First, PVP/BAG composite membranes were produced by electrospinning and the parameters were optimized to produce smaller fibres as it translates into higher surface area and higher bioactivity. IONPs were then incorporated in the solution.

The electrospun membranes were crosslinked due to the PVP water-soluble characteristic. UV and thermal crosslinking were employed, but only thermal crosslinking proved to be successful. For this to be successful TGA/DSC was helpful to find the crosslinking temperature and provided information about the thermal stability of the membranes.

Water-insoluble membranes were tested for magnetic hyperthermia application and cytotoxicity assays were also performed. The IONPs proved to have superparamagnetic properties and a small temperature variation was achieved for a 10 mg membrane sample, which proved the potential of composite membranes for this application.

**Keywords:** Bioactive glass, bone regeneration, composite membranes, iron oxide nanoparticles, magnetic hyperthermia.

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# Contents

<b>Acknowledgements.....</b>	<b>v</b>
<b>Resumo .....</b>	<b>vii</b>
<b>Abstract.....</b>	<b>ix</b>
<b>Contents .....</b>	<b>xi</b>
<b>List of figures.....</b>	<b>xiii</b>
<b>List of tables.....</b>	<b>xv</b>
<b>Abbreviations and symbols .....</b>	<b>xvii</b>
<b>1 Motivation and objectives.....</b>	<b>1</b>
<b>2 Introduction.....</b>	<b>3</b>
2.1 Scientific context.....	3
2.2 Magnetic Nanoparticles.....	3
2.3 Bioactive glasses .....	5
2.4 Silica-based BAG Polymeric Fibrous Membrane .....	5
2.5 Electrospinning technique .....	6
<b>3 Materials and Methods.....</b>	<b>9</b>
3.1 Synthesis of BAG by Sol-Gel and Ball Milling .....	9
3.2 Synthesis of iron oxide nanoparticles stabilized with oleic acid .....	9
3.3 Fabrication of polymeric fibrous magnetic membranes by electrospinning.....	9
3.4 Characterization .....	10
3.5 Magnetic Hyperthermia assays.....	10
3.6 Bioactivity .....	10
3.7 Cytotoxicity Assays.....	10
<b>4 Results and Discussion.....</b>	<b>11</b>
4.1 Preparation of the precursor materials.....	11
4.2 Production of composite membranes by electrospinning .....	13
4.3 Magnetic hyperthermia Assays .....	26
4.4 Bioactivity Assays in SBF.....	26
4.5 Cytotoxicity Assays.....	27
<b>5 Conclusions and future perspectives .....</b>	<b>30</b>
5.1 Future Perspectives.....	31
<b>References .....</b>	<b>32</b>
<b>6 Supporting information.....</b>	<b>34</b>
6.1 Tested electrospinning parameters .....	34

6.2	Procedure for <i>in vitro</i> cytotoxicity evaluation.....	36
6.3	SEM/EDS elements colour trace of composite membranes (PVP/BAG).....	37
6.4	SEM/EDS elements colour trace of composite membranes (PVP/BAG/IONPs).....	38

## List of figures

Figure 2.1. Schematic illustration of (A) a single domain magnetic NP with its magnetization pointing to one direction, (B) a group of single domain magnetic NPs aligned along a magnetic field direction, (C) the hysteresis loop of a group of ferromagnetic NPs, and (D) the hysteresis loop of a group of superparamagnetic NPs. (Adapted with permission from [9]. Copyright 2011 American Chemical Society).....	4
Figure 2.2. Bioactive Glass surface reaction and bone regeneration mechanism [20]. .....	6
Figure 2.3. Schematic illustration of electrospinning setup.....	7
Figure 4.1. Bioactive glass obtained by sol-gel - EISA process using with a structure-directing agent (Pluronic F127).....	11
Figure 4.2. SEM of BAG powders and the respective EDS element spectrum, elements atomic and weight concentration through EDS. The picture was taken in a 15 KV mode with a backscattered electron detector. ....	12
Figure 4.3. FTIR spectra of BAG and Pluronic F127.....	13
Figure 4.4. (left) Representative image of a 18% PVP membrane obtained from the design of experiences study. (right) Corresponding SEM image of the same membrane. The used electrospinning parameters to produce this membrane were 20 kV; 20 cm and 0,1 ml/h. ....	14
Figure 4.5. Sample E2 (a), branched fibres in sample B3 (b), flat fibres in sample D4 (c) and deformed fibres in sample D4 (d) .....	15
Figure 4.6. Particle size distribution of BAG powders before and after 6 h of ball milling process. ....	16
Figure 4.7. SEM image of fibres produced with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solution and the following parameters: 20 kV, 20 cm and 0,15 ml/h (sample 18), and the respective size distribution graph.....	19
Figure 4.8. SEM image of the PVP 14 wt.% and BAG 14 wt.% membrane (top, left), and the respective EDS elemental map (top, right). Normal and atomic Concentration (wt.% and at.%) quantification on the left down image. Element spectrum on the right down image (carbon and oxygen were ignored) (see Figure 6.2 in supplementary information for complete information of the element colour trace). ....	20
Figure 4.9. DSC/TGA of plain PVP membrane (A) and of composite PVP 14 wt.% and BAG 14 wt.% membrane. ....	21
Figure 4.10. SEM image of the PVP 14 wt.%, BAG 14 wt.% and 4% IONPs membrane (top, left), and the respective EDS elemental map. Normal and atomic Concentration (wt.% and at.%) quantification on the left down image. Element spectrum on the right down image (carbon and oxygen were ignored) (see Figure 6.3 in supplementary information for complete information of the element colour trace). ....	22
Figure 4.11. Plain PVP 18 wt.% membranes with different UV crosslinking times after immersed in water. ....	23
Figure 4.12. SEM analysis of the respective PVP 18 wt.% membranes with different UV times in Figure 4.11 after immersed in water. ....	24
Figure 4.13. PVP membrane without treatment before immersion, and PVP membranes with thermal cross-linking of 150°C with different cross-linking times, after immersion (note: To be able to properly observe the structure different magnifications had to be used for each sample, therefore the magnification used should not be considered). ....	24

Figure 4.14. PVP, PVP BG, PVP BG IONP's membranes observed on SEM, before and after crosslinking at 150 °C for 24 h, and after 24 h immersion in ultra-pure water and drying. ....	25
Figure 4.15. Temperature variation (°C) from magnetic hyperthermia assays for IONPs in 4% aqueous solution, 10 and 20 mg of 14 wt.% PVP, 14 wt.% BAG, and 4 wt.% IONPs.....	26
Figure 4.16. SEM images of the PVP 14 wt.% and BAG 14 wt.% after 6, 12, 24, 48 and 72 h immersion in SBF. ....	27
Figure 4.17. Vero cell viability (%) after indirect exposure to the different electrospun membranes. PVP corresponds to plain PVP 18 wt.% membrane; BAG corresponds to composite PVP 14 wt.% and BAG 14 wt.% membrane; and IONPs correspond to composite PVP 14 wt.%, BAG 14 wt.% and IONPs 4 wt.% and respective dilutions 1 and 2 (factor 2).....	28
Figure 6.1. Schematic planning for cytotoxicity assays. ....	36
Figure 6.2. SEM/EDS elements colour trace attached to Figure 4.8. ....	37
Figure 6.3. SEM/EDS elements colour trace attached to Figure 4.10. ....	38

## List of tables

Table 4.1. Average diameter of electrospun fibres obtained from PVP and BAG mixtures. Results are presented as average diameter $\pm$ standard deviation calculated from at least 30 measures. Samples codes (A1 to E8) correspond to a set of electrospinning parameters, which can be consulted in Table 6.1 in supplementary information. ....	14
Table 4.2. Influence of flow rate in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent. ....	17
Table 4.3. Influence of applied voltage in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent. ....	18
Table 4.4. Influence of the needle to collector distance (cm) in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent. ....	18
Table 6.1. Electrospinning parameters tested using different concentrations of BAG in an 18 wt.% PVP solution in ethanol. ....	34
Table 6.2. Set of electrospinning parameters tested using a solution of 14 wt.% PVP and 14 wt.% BAG (both relative to solvent mass) in a mixture of ethanol:water in a ratio of 85:15 (v/v). ....	35





## Abbreviations and symbols

AMF	Alternating magnetic field
ATR	Attenuated total reflectance
BAG	Bioactive glass
Ca	Calcium
CT	Chemotherapy
DMSA	Dimercaptosuccinic acid
DTA	Differential thermal analysis
EDS	Energy dispersive spectroscopy
EISA	Evaporation induced self-assembly
F127	Pluronic F127
Fe <sub>3</sub> O <sub>4</sub>	Magnetite
FTIR	Fourier transform infrared spectrometer
<i>H</i>	Magnetic field
HA	Hydroxyapatite
HT	Hyperthermia
IONPs	Iron Oxide NPs
MBG	Mesoporous bioactive glass
MNPs	Magnetic nanoparticles
<i>M<sub>s</sub></i>	Magnetization saturation
MRI	Magnetic resonance image
Na	Sodium
NP	Nanoparticle
O	Oxygen
OA	Oleic acid
P	Phosphorous
P123	Pluronic 123
PEO	Poly(ethylene oxide)
PVA	Poly(vinyl alcohol)
PVP	Polyvinylpyrrolidone
RT	Radiation Therapy
SAR	Specific absorption rate
SBF	Simulated body fluid

SEM	Scanning electron microscopy
Si	Silicon
TEOS	Tetraethyl orthosilicate
TEP	Triethylphosphate
TGA	Thermogravimetric analysis
UV	Ultraviolet

# 1 Motivation and objectives

Cancer is a global problem with an increasing incidence every year. In particular, bone cancer has a high incidence and related death in young groups. Bone is also the third most frequent site of metastasis, after lung and liver, which reflects the high incidence of bone injuries. Bone cancer treatment usually originates bone defects with residual tumour cells that can proliferate during bone regeneration. Therefore, a scaffold for bone regeneration that simultaneously kill residual tumour cells is needed.

In the Biomaterials group the research is focused in developing new composite materials for biomedical applications. One of the main research areas is the development of multifunctional magnetic nanoparticles for cancer theranostic through a combination of magnetic hyperthermia, controlled drug delivery and diagnostic by magnetic resonance imaging. On another research line, the group has focused on the development of composite materials for bone tissue engineering. More recently, a PhD student started to develop a 3D composite system composed of bioactive glasses (BAGs), magnetic nanoparticles and a capsule of electrospun fibres. This system is highly bioactive and resorbable due to the bioactive glass which leads to formation of a hydroxyapatite layer that bonds to collagen fibrils. The system is biodegradable at an adequate rate for bone regeneration. BAGs are greatly known for their bioactive properties and ability to induce bone and tissue regeneration. They have also been electrospun into fibrous membranes, with suitable diameters and great surface area that further improve their bioactivity when compared to BAG in the form of powder, so a BAG fibrous membrane represents a very good candidate to incorporate the MNPs for hyperthermia treatments. A biocompatible polymer like Polyvinylpyrrolidone (PVP) may be used to help properly produce these membranes, through electrospinning technique. Magnetic nanoparticles act as thermosteeds generating clinically relevant heat under an applied alternating magnetic field to kill or sensitize tumour cells. In combination with release of an anticancer drug, this composite system will effectively kill bone tumour cells whilst providing a base for bone regeneration.

In this thesis the main objective is to produce by electrospinning a composite membrane composed of bioactive glass, a biocompatible and biodegradable polymer with magnetic nanoparticles incorporated. This composite membrane should be bioactive and be suitable for magnetic hyperthermia application, making a proof of concept of a material that can aid the regeneration of bone and simultaneously kills cancer cells by magnetic hyperthermia in the tumour site. To achieve such objective, the following topics were addressed:

- Study the influence of electrospinning parameters in the production of polymer/bioactive glass fibres;
- Optimize bioactive glass concentration (as the bioactive glass will be majorly responsible for the bioactive properties of the composite) in the fibres;
- Successfully incorporate magnetic nanoparticles in the composite membrane, to properly induce magnetic hyperthermia treatment
- Study the biomedical application of the produced composite membranes by performing cytotoxicity studies, bioactivity studies and magnetic hyperthermia studies.



## 2 Introduction

### 2.1 Scientific context

Current cancer treatments are based on surgery, radiotherapy (RT), chemotherapy (CT) and biological therapies [1]. Radiotherapy uses high-energy rays or particles to kill cancer cells, but most bone cancers are not easily killed by radiation, and high doses are needed. This can damage nearby healthy tissues and structures like nerves and blood vessels. Consequently, radiotherapy is not used as a main treatment for most bone tumours, but it is used to slow the growth of cancer cells generated due to bone metastases [2]. Chemotherapy consists in using systemic drugs to kill cancer cells all over the body. This treatment option is limited for larger tumours (like most bone cancers) because the treatment is not localized and healthy cells are very sensitive to current chemotherapy drugs, therefore it is not a very effective method for bone cancer treatment [1], [2].

An alternative treatment that has been studied these past years is hyperthermia (HT) with the help of magnetic nanoparticles (MNPs). Magnetic HT works as a calculated increase of temperature in the human body, within the range of 40–44 °C, by applying an electromagnetic stimulus on magnetic nanoparticles that act like thermoseeds. Their efficiency can be measured by the ability to reach and accumulate on the tumour area [3]. This temperature increase leads to tumour cell death which are more sensitive to heat than normal tissues. Clinical application of hyperthermia is not established as a single treatment modality but as a way to improve chemotherapy and radiotherapy results, when applied in repetitively short intervals [4]–[6].

In order to adequately perform localized magnetic hyperthermia in an affected area it is important to find new alternatives that ensure the presence of NPs in the tumour region without any cytotoxic effect. A biocompatible, bioactive membrane with trapped NPs may represent a good alternative as it avoids the leakage of NPs in the targeted area.

### 2.2 Magnetic Nanoparticles

Magnetic Nanoparticles have been widely studied for biomedical applications as contrast agents for magnetic resonance imaging (MRI) and as hyperthermia agents for cancer treatment. [20]. There are different types of MNPs, generally composed of pure metals, metal alloys or metal oxides. From all of those, Iron Oxide NPs (IONPs) specifically  $\text{Fe}_3\text{O}_4$  (magnetite) have shown superior biocompatibility and stability and are the most commonly used magnetic NPs for biomedical applications. MNPs physicochemical properties are size-dependent and in proper conditions are able to generate heat when subjected to an alternating magnetic field (AMF), due to energy losses during the demagnetization process, which is crucial for HT [7].

A ferromagnetic NP with size smaller than 20 nm often contains a single magnetic domain with one collective magnetization direction (Figure 2.1 A). Once these NPs are placed under an external magnetic field ( $H$ ), their magnetization directions can be aligned along the field direction to achieve magnetic saturation with overall magnetization reaching the saturation magnetization ( $M_s$ ) (Figure 2.1 B and C). When the size of a ferromagnetic NP is reduced to a level where the thermal energy is comparable to the magnetic anisotropy energy, this NP is magnetically unstable and is said to be superparamagnetic[8]. A group of superparamagnetic NPs can be easily magnet-

ized (with large susceptibility) to reach  $M_s$ , but they have no coercivity and remnant magnetization (Figure 2.1 D). Magnetic NPs in the superparamagnetic state have much weaker magnetic dipole interactions and therefore are readily stabilized and dispersed in liquid media [9].

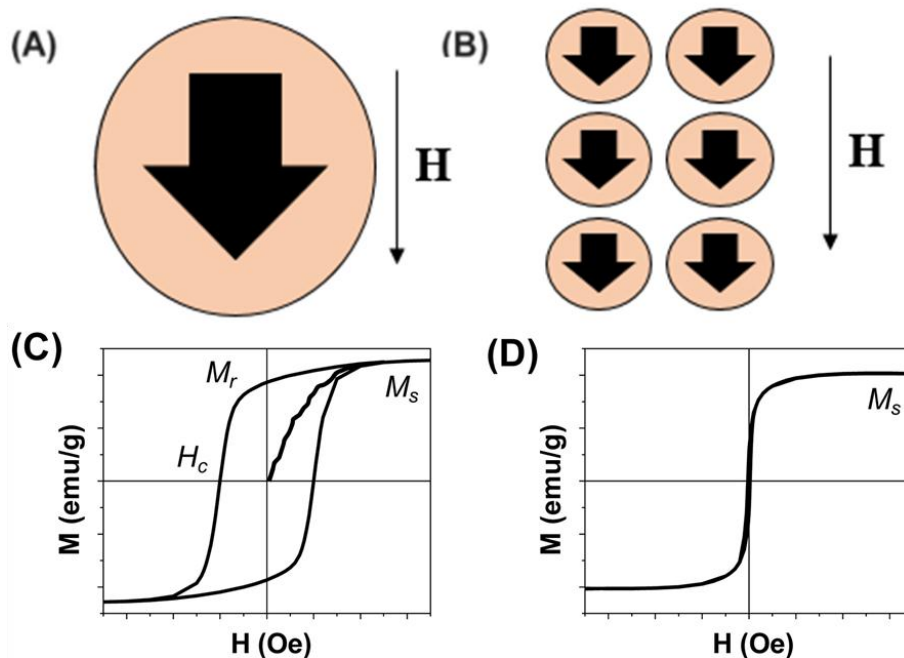


Figure 2.1. Schematic illustration of (A) a single domain magnetic NP with its magnetization pointing to one direction, (B) a group of single domain magnetic NPs aligned along a magnetic field direction, (C) the hysteresis loop of a group of ferromagnetic NPs, and (D) the hysteresis loop of a group of superparamagnetic NPs. (Adapted with permission from [9]. Copyright 2011 American Chemical Society)

The frictions caused by the physical rotation of a NP, Brownian relaxation, and the magnetization reversal within the NP, Néel relaxation, lead to the loss of magnetic energy and the generation of thermal energy. The heating power of these NPs is directly related to the ferromagnetic hysteresis area and frequency of the alternating magnetic field [10]. To ensure better thermal effects under the common hyperthermia conditions, magnetic NPs should have small coercivity, large susceptibility, and high  $M_s$ . The NP heating efficiency is measured by the specific absorption rate (SAR,  $W \cdot g^{-1}$ ). For practical therapeutic applications with minimized side effects, it is critically important to obtain optimum heating efficiency to reach the desired hyperthermia temperature at 41-44 °C [9]. MNPs stability in physiological conditions can limit their desired performance. The size of MNPs is the crucial factor determining their uptake of target cell and elimination from the body. For example MNPs which have the diameter size larger than 200 nm are retained in the spleen and liver while particles of smaller sizes than 10 nm are rapidly removed via renal clearance [3]. In order to avoid that, several reports on MNPs coating with molecules like oleic acid (OA) or dimercaptosuccinic acid (DMSA) have been successful on stabilizing the MNPs and preventing their aggregation as they create repulsive forces, mainly stereo chemical repulsions, that compensate the attractive magnetic and van der Waals forces [4] [7].

## 2.3 Bioactive glasses

Bioactive glasses are a class of biomaterial with increased interest along the years. BAGs form a hydroxyapatite (HA) layer on the biomaterial when implanted in the human body through glass dissolution. HA is the inorganic part of human bone and therefore BAGs are able to bond and form a stable interface with bone tissues while being biodegradable and stimulating bone regeneration [11]–[13]. The first form of BAG was Larry Hench's 45S5 Bio-glass (commercial name) with a 45 wt.% SiO<sub>2</sub>, 24.5 wt.% CaO, 24.5 wt.% Na<sub>2</sub>O, and 6.0 wt.% P<sub>2</sub>O<sub>5</sub> composition (wt.% represents the molecular weight percentage), produced by a melt quenching synthesis and presented in the late 1960's [11]. Since then, many different compositions of bio-glass and their *in vitro* and *in vivo* behaviour has studied.

There are different techniques available in literature to produce BAG. Melt quenching is a process that requires temperatures up to 1300-1400 °C and only bio glasses produced with less than 60 wt.% of SiO<sub>2</sub> show bioactivity in *in vivo* conditions. Above that level of wt.% of SiO<sub>2</sub> the material does not develop a HA layer and does not bond to bone or soft tissues. The major alternative process to melt quenching is the Sol-Gel technique which is a lower temperature process. This process enables the production of a larger range of bio glass compositions, up to 90 wt.% SiO<sub>2</sub>, with similar biological response to the ones produced by melt quenching [14], [15]. Sol-gel BAGs exhibit higher rates of apatite phase formation, faster bone bonding and excellent degradation and resorption properties [16].

In order to enhance bioactivity, both composition and structure are important in BAGs derived from sol-gel. A better control of properties like specific surface area and pore volume can increase the bioactive response, so it is important to control the overall porosity and pore structure of the material. In 2004, Yan *et al.* [13] pioneered the synthesis of mesoporous BAGs with SiO<sub>2</sub>-CaO-P<sub>2</sub>O<sub>5</sub> system, breaking ground for the development of BAGs with superior bioactivity compared to conventional melt-derived and sol-gel materials.

## 2.4 Silica-based BAG Polymeric Fibrous Membrane

In order to induce proper bone regrowth, the materials that compose the scaffold must be biocompatible and the scaffold itself should provide proper environment to stimulate new bone production. Allowing cells and blood vessels to spread through the scaffold is very important and for that, a certain level of macro/microporosity is necessary.

Silica-based BAGs are able to bond and create a stable interface with living bone tissue without promoting inflammation or toxicity [17]. Their main advantage to be used in bone regeneration is their high bioactivity, which allows BAGs to create an apatite-like phase, similar to the inorganic part of the bone, when in contact with physiological fluids. Also the degradation of these BAGs have shown osteoconductive properties, which means that bone tissue grows on BAG surface [18], [19]. The reaction at BAG surface when in contact with body fluids is illustrated in Figure 2.2 and described elsewhere [20].

In order to produce BAGs with high surface area and high porosity at low temperatures, both crucial for high bioactivity, the sol-gel process has been widely used and studied along the years. During the sol-gel process, the gelling stage occurs at room temperature. Bioactive glasses can be made by sol-gel processing, thus facilitating the incorporation of organic and biological

molecules within the network, or even cells within silica matrices [18]. Moreover, sol–gel processes can be combined with supramolecular chemistry of surfactants, resulting in a new highly ordered mesoporous material for biomedical applications. Yan *et al.* [13] compared conventional sol-gel BAGs to new sol-gel BAGs with non-ionic triblock co-polymers Pluronic 123 and Pluronic 127 assisted by Evaporation Induced Self-Assembly (EISA). The EISA process is based on preferential evaporation of the solvent which progressively enriches the concentrations of non-volatile solution constituents and finally ordered mesophase occurs. The surfactant molecules self-organize into micelles that link the hydrolysed silica precursors through the hydrophilic component and self-assemble to form an ordered mesophase [21]. After gelling, drying and surfactant calcinations, bioactive mesoporous glasses (MBG) were obtained. It was also revealed by scanning electron microscopy (SEM) analysis that the bioactivity of MBG strongly depends on MBG composition. 80S15Ca5P MBG showed a bigger bioactivity than 70S25C5P, 60S35C5P, 100S by decreasing order [13].

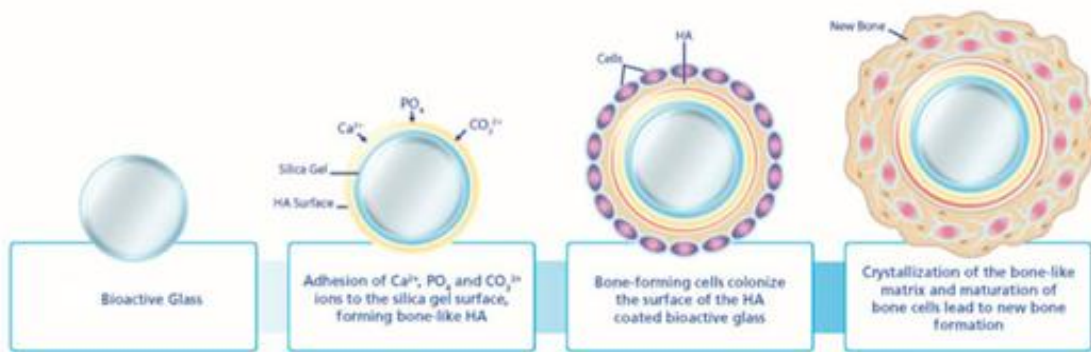


Figure 2.2. Bioactive Glass surface reaction and bone regeneration mechanism [20].

Among the different BAG structures produced, MBGs of nanofibrous structure present two advantages: at microscopic level the ultrathin fibres have highly specific surface areas and at macroscopic scale, due to their long length, the nanofibres can be assembled in 3D membranes with an interconnected macroporous network [22], [23].

## 2.5 Electrospinning technique

Nano fibrous membranes can be obtained by several techniques such as drawing, templates synthesis, phase separation, self-assembly and electrospinning [22]. From these, electrospinning stands out as being the most accessible, versatile, low cost and relatively fast compared to the previous mentioned techniques.

Electrospinning is a broadly used technology for fibre formation which uses electrical forces to produce nano or micro polymer fibres. In a conventional electrospinning setup (Figure 2.3), the solution passes through a needle and a high voltage is applied. At a critical voltage the repulsive force of the charged particles within the solution, overcomes the surface tension of the solution and a jet erupts from the tip of the needle towards a grounded collector. The fibres morphology will depend on the solution properties (viscosity, conductivity and surface tension); flow rate of the solution, voltage applied to the needle, distance between the needle and collector and



finally temperature and humidity. Electrospinning requires a viscoelastic solution that has the ability to stretch under high elongation forces, while resisting break-up, so the use of a polymer like PVA, PVP or PEO is often needed in order to guarantee electrospun fibres [24].

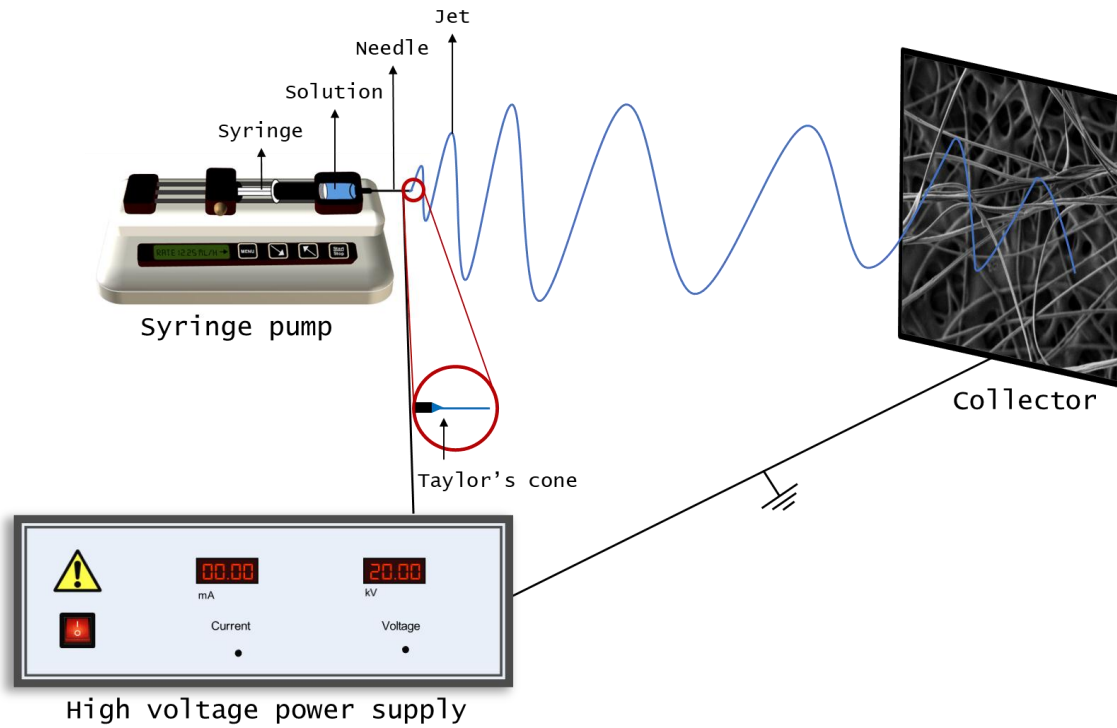


Figure 2.3. Schematic illustration of electrospinning setup.



## 3 Materials and Methods

### 3.1 Synthesis of BAG by Sol-Gel and Ball Milling

BAG powders were produced by a simple sol-gel process assisted by EISA using tetraethyl orthosilicate ( $C_4H_{20}O_4Si$ , TEOS, *Sigma-Aldrich*), calcium nitrate ( $Ca(NO_3)_2$ , *VWR Chemicals*), and triethyl phosphate ( $(C_2H_5O)_3PO$ , TEP, *Fluka*) as inorganic precursors, Pluronic F127 (Mw 12000 Da, *Sigma-Aldrich*) as the structure-directing agent, and ethanol (*Sigma-Aldrich*, 99.8%) as solvent. The amount of inorganic precursors was calculated in order to obtain a ratio of 80Si:15Ca:5P (representing the molar fraction of Si, Ca and P).

The process was adapted from the work of Yan [13]. First, 1.84 g of F127 were dissolved in a 60 g of ethanol. 6.7 g TEOS, 0.73 g TEP and 1.4 g  $Ca(NO_3)_2$  were added in this order, with a 1 ml of 0,5 M HCl solution being added at last. The final solution was kept at room temperature under magnetic stirring for 24 h. To completely dry the gel, the resulting sample was kept at 60 °C until total evaporation of ethanol. The final mesostructured product was shattered by a ball milling technique using the Planetary Mono Mill “pulverisette 6”, Fritsch for 6 h. The powders were uniformly grinded by planetary ball mill, with zirconia balls with 1500 RPM in grinding periods of 30 min, to avoid the equipment overheating. At last, the powders were left to dry and were prepared. Measures of the powder were taken before and after 6 h of grinding.

### 3.2 Synthesis of iron oxide nanoparticles stabilized with oleic acid

IONPs were produced by chemical co-precipitation technique as described by Matos *et al.* [4]. Iron chloride tetrahydrate ( $FeCl_2 \cdot 4H_2O$ , 2.5 mmol, *Sigma-Aldrich*) and iron chloride hexahydrate ( $FeCl_3 \cdot 6H_2O$ , 5 mmol, *Sigma-Aldrich*) were mixed in ultrapure water (*Mili-Q*) followed by addition of an ammonium solution ( $NH_4OH$  at 25 %, 10 ml, *Panreac*) to precipitate the IONPs in the absence of oxygen (by bubbling  $N_2$ ). The amount of oleic acid was calculated as a percentage of the NPs mass [7], followed by ultrasonic bath during 3 h to ensure the coating of all IONPs. To remove the excess of oleic acid, the suspension was in dialysis until pH 7.

### 3.3 Fabrication of polymeric fibrous magnetic membranes by electrospinning

The electrospinning solution was prepared using polyvinylpyrrolidone (PVP, Mw 1 300 000 Da, *Sigma-Aldrich*) as an auxiliary polymer to adjust the solution viscosity and to promote fibre formation [25]. A 14 wt.% BAG and 14 wt.% PVP (both relative to ethanol mass) solution was prepared using magnetic stirring and ultrasounds to uniformly disperse the BAG particles. The high voltage source used for the electrospinning process was a Glassman EL 30kV, which was connected to the metal needle through the positive pole, and the ground with the collector. The infuser pump, which had a constant flow rate, was a KDS100 KD Scientific. The solution was always carefully introduced into a 1 ml syringe, with an internal diameter of 4.50 mm. As for the metal needles used, a 21 G gauge needle was always used in this work. The fibres were collected on an aluminium foil, with the collector being motionless. All equipment was wrapped in an acrylic box for a better control over the environmental parameters of the process,

with the natural humidity of the laboratory being around 30-40%. Fibres production was optimized by varying the flow rate, applied voltage and distance to the collector at controlled humidity and temperature (Table 6.1 in Supplementary information). Furthermore, IONPs were added to the ethanol/PVP/BAG system to achieve a 4 wt.% IONPs (wt.% relative to the polymer mass).

PVP is highly soluble in water and therefore not suitable for biological applications. Therefore, PVP membranes were crosslinked by thermal crosslinking with temperatures of 150 °C, 175 °C and 200 °C for times of 5, 10, 15, 20 and 24 h using the Nabertherm High Temperature Furnace HTCT 01/16/P330 LC011H6SN and also by UV radiation crosslinking using a Vilber Lourmat™ Biolink™ BLX UV Crosslinker for 1, 2, 3, 4, 5 and 6 h.

### 3.4 Characterization

Scanning electron microscopy (SEM) was performed using a Carl Zeiss Auriga SEM equipment to analyse fibre morphology. The samples were coated with a thin layer of gold and palladium. Additionally, Energy Dispersive Spectroscopy (EDS) using Oxford Instruments EDS was performed to detect the presence of BAG and iron elements in the fibres. FTIR spectra of the samples were obtained using a Nicolet 6700–Thermo Electron Corporation Attenuated Total Reflectance-Fourier Transform Infrared spectrometer (ATR-FTIR). Measurements were performed in freeze-dried samples in the range of 480–4000  $\text{cm}^{-1}$  with a resolution of 2  $\text{cm}^{-1}$ . Thermogravimetric analysis (TGA) and differential thermal analysis (DTA) studies were carried out using a Thermal Analyzer NETZSCH STA 449 F3 Jupiter® at a rate of 10  $^{\circ}\text{C}\cdot\text{min}^{-1}$  in a  $\text{N}_2$  atmosphere.

### 3.5 Magnetic Hyperthermia assays

Magnetic hyperthermia measurements were obtained using the equipment NanoScale Bio-magnetics, DM100 Series. The heating capacity of 10 mg of the membranes immersed in 1 ml of ultrapure water with incorporated IONPs were tested. Measurements were performed for 10 min maintaining the magnetic flux density at 24  $\text{kA}\cdot\text{m}^{-1}$  and the frequency at 418.5 kHz.

### 3.6 Bioactivity

Simulated body fluid (SBF) was prepared according to the procedure given by Kokubo *et al.* [26], [27]. Square samples of 1  $\text{cm}^2$  and 5 mg were immersed in 20 ml of SBF for 6, 12, 24, 48 and 72 h. During this time, the samples were placed in an incubator at 37 °C to mimic physiological temperature. After the stipulated time, samples were removed and washed with Millipore water and dried in air. The samples were then observed in SEM.

### 3.7 Cytotoxicity Assays

To evaluate the cytotoxicity of the membranes, the assays were performed according to standard ISO-10993 Biological evaluation of medical devices, Part 5: Tests for *in vitro* cytotoxicity. The assays were performed using the extract method and Vero cells (monkey renal epithelial cells), as described elsewhere [4] and in the section 6.2 of supplementary information in detail.

## 4 Results and Discussion

### 4.1 Preparation of the precursor materials

The main objective of this thesis was to produce and characterize magnetic bioactive glass membranes and to test their application in magnetic hyperthermia. For that, two main precursor materials were used: iron oxide nanoparticles and bioactive glass.

#### 4.1.1 Iron oxide nanoparticles

The IONPs used to produce the fibrous membrane were synthesized using a co-chemical precipitation technique that was previously optimized by the research group [28]. Due to the NPs low stability in aqueous solutions, they were coating with oleic acid. These NPs were extensively characterized in another published work [4]. For some contextualization, we present the most relevant results for this dissertation. Uncoated IONPs are spherical and have an average diameter of  $9.4 \pm 1.9$  nm. The coating of these NPs with oleic acid did not show any influence in particles size or morphology. IONPs crystallinity was studied by XRD showing the presence of magnetite characteristic peaks with a crystalline cubic structure. Again, the presence of the surfactants did not alter the crystalline structure of the IONPs.

#### 4.1.2 Bioactive glass 80Si15Ca5P

In this work BAG was produced by sol-gel technique assisted by EISA using Pluronic F127 as the structure-directing agent. The amount of inorganic precursors was calculated to obtain a ratio of 80Si:15Ca:5P (representing the molar fraction of Si, Ca and P). Figure 4.1 illustrates the obtained BAG which behaves like a gel and can be easily extruded by a syringe.

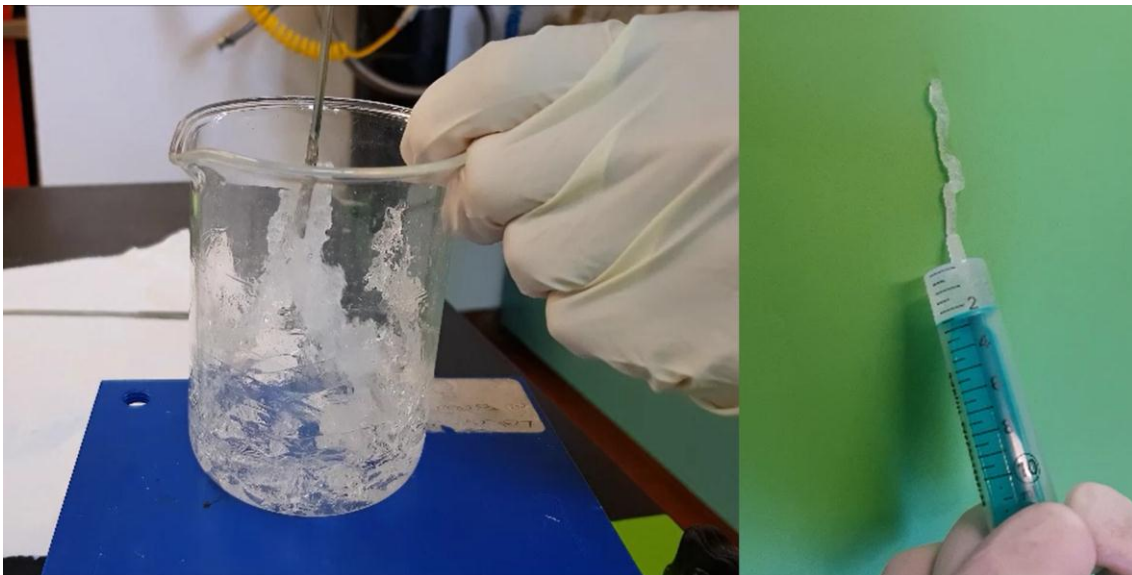


Figure 4.1. Bioactive glass obtained by sol-gel - EISA process using with a structure-directing agent (Pluronic F127).

The first step to characterize the obtained BAG was to confirm its atomic composition, i.e., to confirm if the final molar ratio was 80Si:15Ca:5P. For that, BAG powder was observed with SEM and EDS not only to analyse its structure but also to evaluate the composition elements and atomic concentration of BAG. Figure 4.2 represents SEM image of as-produced BAG and the respective EDS analysis through the element spectrum, the atomic and weight % of each element.

In the SEM image BAG powder shows different particle sizes. The powder does not seem to present any kind of porosity, because unlike most common BAG, this one is not sintered to remove the structural agent. The EDS element spectrum confirms that the as-synthesized BAG is composed by Si, Ca, P, O and C. To determine the weight concentration of Si, Ca and P (the elements responsible for the BAG properties), the elements O and C were ignored. Consequently, an 80,02 % of Si, 16,34 % of Ca and 3,65 % of P atomic composition was confirmed which is very similar to the desired ratio of 80Si:15Ca:5P.

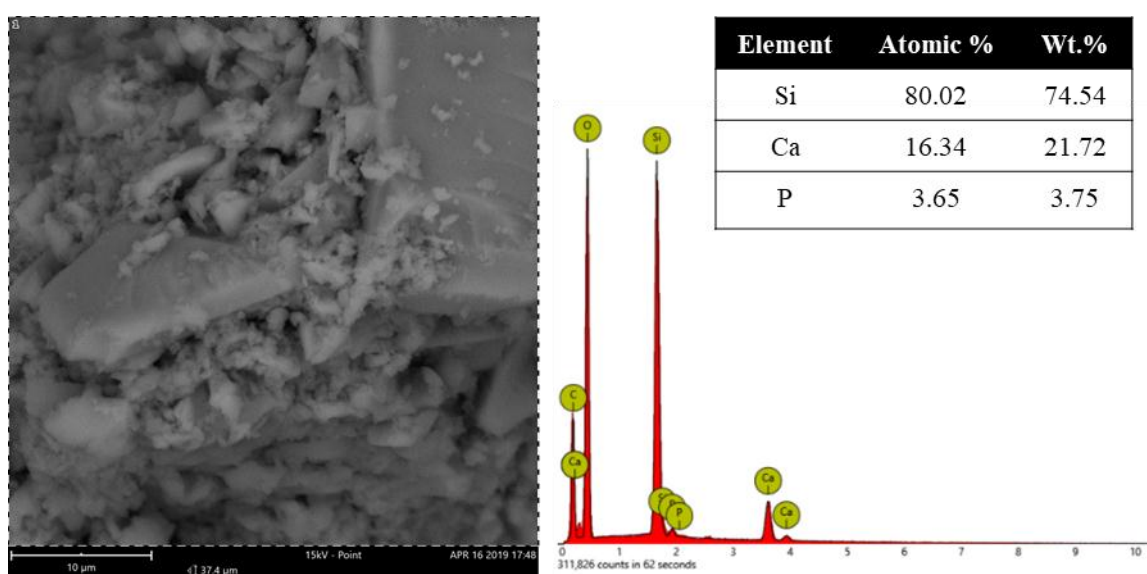


Figure 4.2. SEM of BAG powders and the respective EDS element spectrum, elements atomic and weight concentration through EDS. The picture was taken in a 15 KV mode with a backscattered electron detector.

To analyse the chemical composition of BAG powders, FTIR analysed was performed. Figure 4.3 shows the comparison of BAG and Pluronic F127 spectrum. In BAG spectrum, the band at  $566\text{ cm}^{-1}$  is assigned to the Si-O-Si rocking mode, while the band at  $788\text{ cm}^{-1}$  is attributed to the  $\text{SiO}_4$  bending vibration. The band at  $956\text{ cm}^{-1}$  may be attributed to the Si-OH bending vibration but it is unclear due to a similar peak in Pluronic F127. Moreover, the band at  $1025\text{ cm}^{-1}$  is associated with the  $\text{PO}_4^{3-}$  asymmetric stretching mode (characteristic of BAG), while the band at  $1090\text{ cm}^{-1}$  is usually assigned to the Si-O-Si stretching vibration, however F127 also has a similar band in the same wavenumber. The band in  $1340\text{ cm}^{-1}$  is an O-H in-plane bending characteristic of F127. Finally, the band at  $1645\text{ cm}^{-1}$  is assigned to the stretching vibrations of surface adsorbed water. At  $2890\text{ cm}^{-1}$  a small band is attributed to the  $\text{OH}^-$  stretching mode.

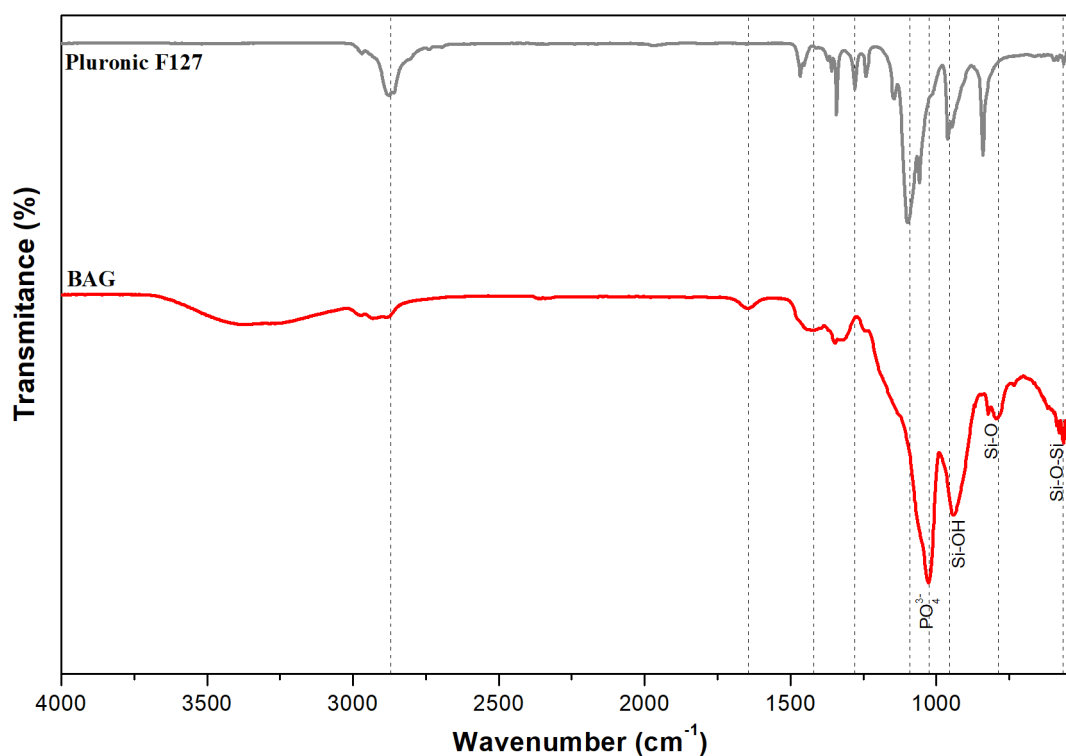


Figure 4.3. FTIR spectra of BAG and Pluronic F127.

## 4.2 Production of composite membranes by electrospinning

Initially, a study was carried out to evaluate the parameters effect on the electrospinning process (applied voltage, flow rate and needle-collector distance) to determine the ideal parameters for the production of PVP membranes. This work was made in parallel by a PhD. student using the design of experiences and the response surface methodology to obtain the smaller fibre diameter. In this work, the smaller diameters are considered the most suitable because smaller fibre diameter leads to higher surface area which is directly related to a higher bioactivity/biodegradation. Figure 4.4 shows the 18 wt.% PVP membrane produced in the referred study and the respective SEM image with an average fibre diameter of  $668 \pm 191$  nm. The electrospinning parameters 20 kV, 20 cm and 0,10 ml/h were taken into consideration while choosing the test parameters for the composite membranes of PVP and BAG.

### 4.2.1 Composite membranes of PVP and BAG

Based of the best set of parameters obtained from the previous study, the composite membranes of PVP and BAG were produced using a PVP concentration of 18 wt.% with different BAG concentrations (1; 2; 3; 4; and 5 wt.%). The main purpose of this step was to evaluate BAG effect on fibres morphology and electrospinning conditions. For this set of experiences 2 flow rates ( $0.2$  and  $0.4 \text{ ml}\cdot\text{h}^{-1}$ ); 2 applied voltages (15 and 20 kV) and 2 different needle-collector distances (15 and 20 cm) were used with controlled humidity and temperature during 15 min of fibre deposition. The average fibre diameters were obtained from SEM images using *ImageJ Software*, by measuring at least 30 single fibres from each collected image. The average fibre diameters are

presented in Table 4.1 and the complete information (correspondence between sample code (A-E) and tested parameters) can be consulted in Table 6.1 in supplementary information.

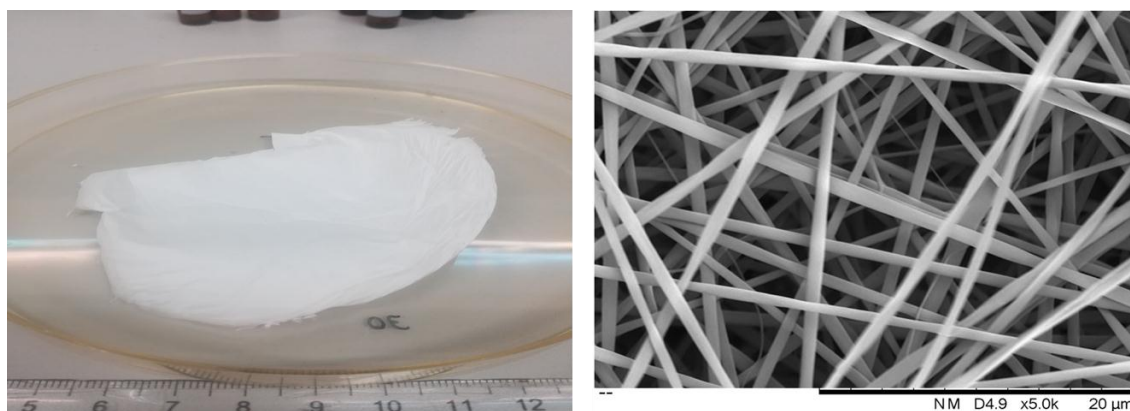


Figure 4.4. (left) Representative image of a 18% PVP membrane obtained from the design of experiences study. (right) Corresponding SEM image of the same membrane. The used electrospinning parameters to produce this membrane were 20 kV; 20 cm and 0,1 ml/h.

Table 4.1. Average diameter of electrospun fibres obtained from PVP and BAG mixtures. Results are presented as average diameter  $\pm$  standard deviation calculated from at least 30 measures. Samples codes (A1 to E8) correspond to a set of electrospinning parameters, which can be consulted in Table 6.1 in supplementary information. (The blank spots represent samples that were not possible to properly visualize with this technique)

Sample	Average diameter (nm)	Sample	Average diameter (nm)	Sample	Average diameter (nm)
A1		C1	336 $\pm$ 72	E1	365 $\pm$ 51
A2		C2	426 $\pm$ 128	E2	360 $\pm$ 56
A3	483 $\pm$ 144	C3	426 $\pm$ 107	E3	368 $\pm$ 125
A4	457 $\pm$ 104	C4	474 $\pm$ 148	E4	374 $\pm$ 60
A5	354 $\pm$ 69	C5	325 $\pm$ 64	E5	421 $\pm$ 67
A6	349 $\pm$ 101	C6		E6	337 $\pm$ 53
A7	368 $\pm$ 87	C7	405 $\pm$ 121	E7	
A8	349 $\pm$ 115	C8	399 $\pm$ 77	E8	
B1	383 $\pm$ 94	D1	350 $\pm$ 63		
B2	353 $\pm$ 90	D2	373 $\pm$ 95		
B3	531 $\pm$ 175	D3	442 $\pm$ 87		
B4	433 $\pm$ 115	D4	409 $\pm$ 108		
B5	411 $\pm$ 131	D5	347 $\pm$ 70		
B6	342 $\pm$ 82	D6	446 $\pm$ 95		
B7	490 $\pm$ 141	D7	308 $\pm$ 45		
B8	396 $\pm$ 107	D8	412 $\pm$ 94		

The number of samples with different electrospinning parameters is too low to determine the ideal conditions. However, it is possible to say that the parameters 15 kV, 15 cm and 0,2 ml/h (samples A1, B1, C1, D1, E1) produced, on average, smaller diameters with a smaller standard



deviation, which means higher uniformity. No significant differences were found samples with different BAG wt. % using the same electrospinning conditions. This indicates that it is possible to increase BAG concentration without significantly affect the average fibre diameter.

However, some defects were found in the composite fibres with the increase of BAG concentration. Most samples presented fibres with regular shape, but some dispersed BAG particles (Figure 4.5 (a)) were visible in some areas of the membrane. Moreover, were also found branched fibres (Figure 4.5 (b)), plane fibres (Figure 4.5 (c)), and deformed fibres (Figure 4.5 (d)). The humidity percentage was lower than 30 % for all these samples. In a low humidity environment, the ejected solvent can evaporate too quickly and cause the phenomenon responsible for these irregular fibres described in literature [29]. Higher applied voltages (around 20 kV) can also cause some electrical instability that could also explain these deformations [29]. In addition, BAG particles are not very well dispersed in the membrane and there is a big discrepancy between particles sizes as it is observed in Figure 4.5 (a) and (d).

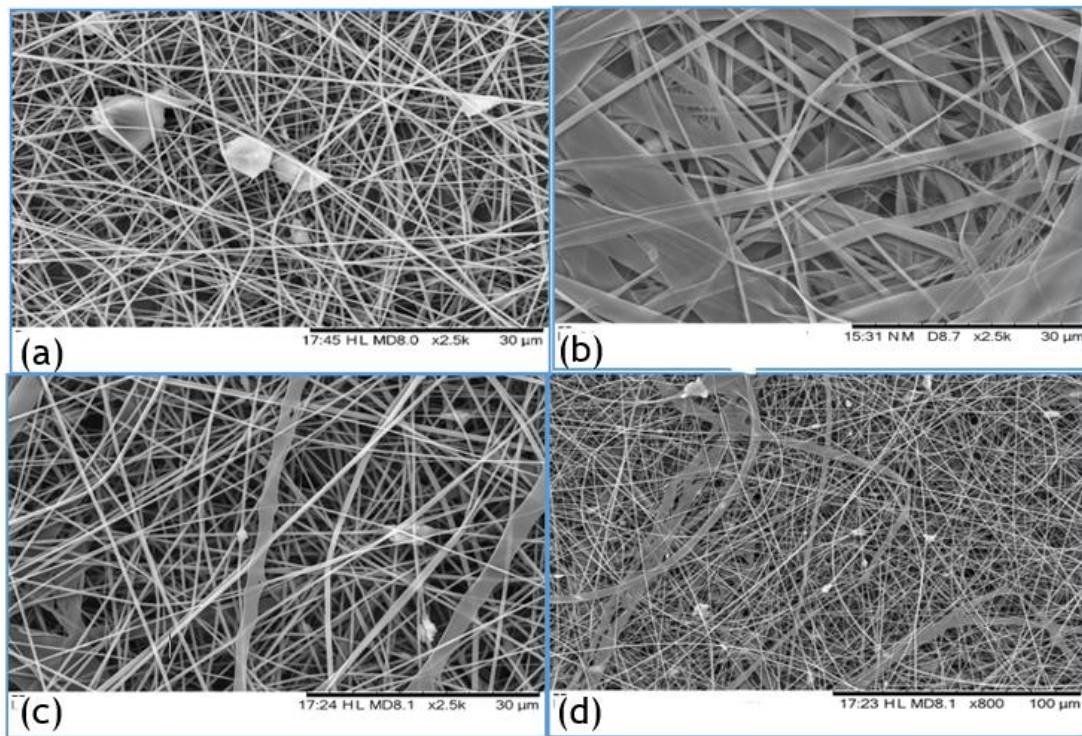


Figure 4.5. Sample E2 (a), branched fibres in sample B3 (b), flat fibres in sample D4 (c) and deformed fibres in sample D4 (d)

From this analysis, it was concluded that the humidity levels should be slightly higher, above 30 % to avoid fibre defects. Moreover, BAG concentration can be increased at least up to 5 wt.%; however, particles should have uniform sizes and should be more dispersed within the membrane.

The higher dispersity of particles in the membrane can be explained by particle size. After complete drying, BAG powders were manually grinded using a grinder and mortar. Using this procedure, the obtained BAG particles had a particle size of around 549  $\mu\text{m}$ . This powder was further incorporated into the electrospun solution. However, after these initial attempts of producing the electrospun membranes, it was obvious through SEM analysis that the BAG particles

size had to be reduced, to promote the homogeneous dispersion of BAG in the membrane. To reduce particle size a ball mill process was used for 6 hours. The particle size analyser proved the particle size reduction from 549  $\mu\text{m}$  (before) to 26  $\mu\text{m}$  (after 6 h), which is represented in Figure 4.6. Although some aggregates are still present, the average particle size was greatly reduced to a factor of around 20 times its initial size.

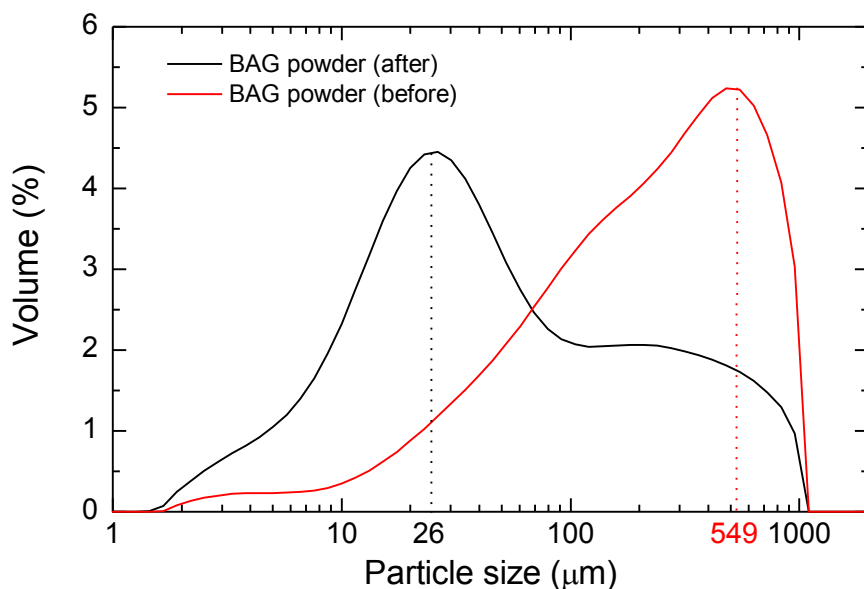


Figure 4.6. Particle size distribution of BAG powders before and after 6 h of ball milling process.

After realizing that BAG content in the electrospun solution could be increased, a solution of 18 wt.% PVP with 9 wt.% BAG was prepared and electrospun. Using an optical microscope, the presence of electrospun fibres were confirmed. Since a content of 9 wt.% of BAG was easily dispersible in the 18 wt.% PVP solution, a test was made by doubling BAG concentration. The prepared solution with PVP and BAG at 18 wt.% each was extremely hard to disperse and with a unsuitable viscosity for electrospinning. Therefore, both PVP and BAG concentration was brought down to 14 wt.% each. This was an easily dispersible solution but when tested in electrospinning, the solvent (ethanol) was evaporating too quickly, not allowing a proper fibre deposition. Consequently, instead of forming a membrane, this solution produced a 3D structure. Since this was not the purpose of this thesis, the solvent was changed to a mixture of ethanol:water in a ratio of 85:15 (v/v). Since the concentrations and solvent were changed, the electrospinning parameters were again optimized to obtain fibres without defects and with the smallest diameter. The set of experiments, as well as the studied parameters can be found in and Table 6.2 in supplementary information. The criteria for choosing the flow rates (0.05; 0.15; 0.25 ml/h) was based on the droplet accumulation on the needle tip. These droplets are to avoid in an ideal electrospinning process, as they can cause big defects on the membrane if the droplet is ejected. If the droplet is not ejected from the needle, this represents a waste of solution and proves the non-ideal efficiency of the process. The applied voltage and needle-collector distance were kept at 15 and 20 kV and 15 and 20 cm, respectively, with intermediate values of 18.3 kV and 18 cm.

The fibres diameters were measured in the same way as before and the results were arranged to facilitate the comprehension of the influence of each process parameter. Table 4.2

shows the influence of flow rate in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent. At a flow rate of 0.25 ml/h a droplet on the needle tip starts to form, which causes instability of the ejected fibres and can explain why there is a tendency to produce higher fibre diameters. Using lower flow rates (0,05 ml/h) smaller fibres are obtained when compared to a flow rate of 0.15 ml/h. Higher flow rates mean more material being ejected with slower drying time, prior to reaching the collector and lower stretching forces, thus explaining higher diameters. Although 0.05ml/h seems the best flow rate for this work purpose, it takes too long to produce a 100 mg membrane. With a 0.15ml/h flow rate that times decreases 3 times, and combined with the 20 kV, 20 cm or 15 kV and 18 cm it can produce good quality fibres with smaller diameter and smaller standard deviation (around  $410 \pm 134$  and  $380 \pm 85$  nm, respectively).

Table 4.2. Influence of flow rate in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent. (The diameters were compared from left to right with the respective colours)

Applied Voltage (kV)	Distance (cm)	Flow Rate (ml/h)		
		0.05	0.15	0.25
15	15			475 ± 90
	18	449 ± 102	380 ± 85	455 ± 123
	20	402 ± 116	470 ± 95	508 ± 108
18,3	15	561 ± 334	603 ± 232	537 ± 382
	18	518 ± 209	486 ± 122	544 ± 196
	20	417 ± 122	457 ± 188	536 ± 138
20	15	558 ± 219	616 ± 204	722 ± 204
	18	520 ± 142	608 ± 196	679 ± 377
	20	548 ± 274	410 ± 134	741 ± 353
		Smaller Diam.	Intermediate Diam.	Higher Diam

Table 4.3 shows that influence of applied voltage in the average fibre diameter (nm) of samples with the same precursor solution. A lower applied voltage usually is responsible for smaller diameters and lower standard deviation. However, this subject is a little controversial, as researchers have proven that voltage does influence fibre diameter, but the level of significance varies with solution viscosity and needle-collector distance [30]. This can explain what happens on the samples with 0.15 ml/h and 20 cm, where the diameters increase with the increase of applied voltage. Besides, with 15 kV a droplet on the needle tip was also formed which can represent a significant waste of electrospinning solution. Finally, Table 4.4 shows the influence of the needle to collector distance (cm) in the average fibre diameter of samples with the same precursor solution. With the increase of needle to collector distance from 15 cm to 20 cm, fibres become thinner, as the ejected solvent has enough time to evaporate before reaching the collector and more time to stretch the fibre.

From this study it can be concluded that for the solution of PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol: water solvent the flow rate of 0.05 ml/h produces the smallest average fibre diameter. However, it takes too long to produce a membrane compared to higher flow rates of 0.15 ml/h and 0.25 ml/h. Of these two, 0.15 ml/h shows the smallest average fibre diameter compared to the ones from 0.25 ml/h. In terms of distance from needle to collector, 20 cm is the best

parameter (compared to 15 and 18 cm) to produce smallest fibre diameter, as well as it decreases the standard deviation, which means a more homogeneous membrane. This is due to the ejected solution having more time to elongate. Regarding the applied voltage, 15 kV produces smaller fibres, but most of the electrospinning solution is not properly ejected, as the voltage is not enough to overcome the surface tension of the solution, and it accumulates on the tip of the needle in form of droplets. The droplets may cause defects on membrane if ejected to the collector, and if not ejected it ends up being material wasted. For this reason, an applied voltage of 15 kV is too be avoided. Fixing the flow rate on 0,15 ml/h and the distance in 20 cm, it is clear that a 20 kV voltage produces better fibres than 18.3 kV.

Table 4.3. Influence of applied voltage in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent.

Flow Rate (ml/h)	Needle-Collector Distance (cm)	Applied Voltage (kV)		
		15	18.3	20
0.05	15		561 ± 334	558 ± 219
	18	449 ± 102	518 ± 209	520 ± 142
	20	402 ± 116	417 ± 122	548 ± 274
0.15	15		603 ± 232	616 ± 204
	18	380 ± 85	486 ± 122	608 ± 196
	20	470 ± 95	457 ± 188	410 ± 134
0.25	15	475 ± 90	537 ± 382	722 ± 204
	18	455 ± 123	544 ± 196	679 ± 377
	20	508 ± 108	536 ± 138	741 ± 353

Table 4.4. Influence of the needle to collector distance (cm) in the average fibre diameter (nm) of samples with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solvent.

Applied Voltage (kV)	Flow Rate (ml/h)	Needle-collector distance (cm)		
		15	18,3	20
15	0.05		449 ± 102	402 ± 116
	0.15		380 ± 85	470 ± 95
	0.25	475 ± 90	455 ± 123	508 ± 108
18.3	0.05	561 ± 334	518 ± 209	417 ± 122
	0.15	603 ± 232	486 ± 122	457 ± 188
	0.25	537 ± 382	544 ± 196	536 ± 138
20	0.05	558 ± 219	520 ± 142	548 ± 274
	0.15	616 ± 204	608 ± 196	410 ± 134
	0.25	722 ± 204	679 ± 377	741 ± 353

For these reasons, the parameters 0,15 ml/g flow rate; 20 cm distance and 20 kV applied voltage, were the chosen for producing the membranes as depicted in Figure 4.7. The membrane produced with these parameters had a average fibre diameter of  $410 \pm 169$  nm with (what appears to be) small nuclei of BAG within. Some reports like [31] have achieved similar sizes in their studies. Most of fibres measured have diameters between 300 and 400 nm, however there are still

some fibres with over 700 nm, which increases the standard deviation and may be attributed to the high voltage (20 kV) used in the process. Compared to the 18% PVP membranes in the DOE referred above, these PVP, BAG membranes had smaller diameters for similar parameters. This may be attributed to the smaller PVP concentration (14 wt.%) in the PVP, BAG membranes, as it has been shown that solutions with lower polymeric concentration produce smaller fibre diameters [31].

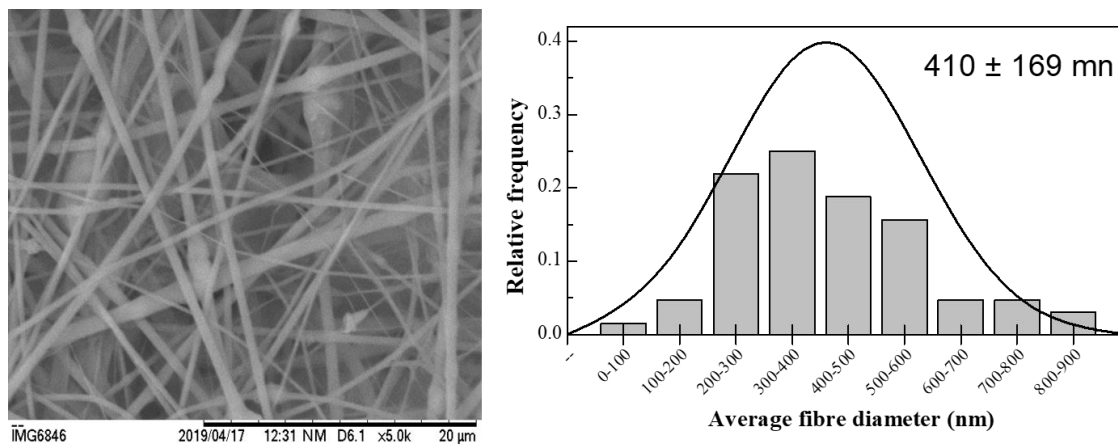


Figure 4.7. SEM image of fibres produced with PVP 14 wt.% and BAG 14 wt.% in an 85:15 ethanol:water solution and the following parameters: 20 kV, 20 cm and 0,15 ml/h (sample 18), and the respective size distribution graph.

After the optimization of the electrospinning parameters, the composition of the obtained membranes was analysed. First, with the help of EDS equipment coupled to SEM, the atomic concentration and element maps were analysed to examine the presence of BAG within the fibrous scaffold. Figure 4.8 shows the SEM image of the PVP 14 wt.% and BAG 14 wt.% membrane and the respective EDS elemental map. Analysing SEM image it is clear the presence of round shaped BAG particles trapped and mixed in the fibrous scaffold. These nuclei are majorly composed of silica, with presence of calcium and phosphorous. Ca and P also seem to be dispersed within the polymeric fibres. EDS also provides the quantification of both normal concentration and atomic concentration of the elements present on the spectrum (Figure 4.8 down right image). The atomic composition, 74.84 wt.% of Si, 17.64 wt.% of Ca and 7.66 wt.% of P is very close to the desired 80Si15Ca5P composition.

Thermogravimetric analysis was carried out to study the thermal stability of PVP and the composite membranes. TGA of the PVP membrane (Figure 4.9 A) showed the first mass loss below 100 °C corresponding to the 56 °C exothermic peak in the DSC trace. This is associated with water adsorption and other alcohol by-products of the condensation reactions. A small mass loss continues until 340 °C occurs, and the exothermic peak 185 °C is believed to be related to the PVP reticulation, as it has been reported to be around between 150 °C and 200 °C [31]. Only at around 340 °C PVP starts decomposing until around 460 °C where only a residual mass percentage is left. Analysis of the thermal stability of composite membranes in Figure 4.9 B shows a first mass loss of 5.11 % until around 120 °C corresponding to the exothermic peak at 59 °C, which is attributed to the water adsorption and other alcohol by-products of the condensation reactions. A new mass loss of 122 % occurs from 120 °C until around 380 °C. From 150 °C to 200 °C the mass loss can be attributed to the PVP crosslinking, as it has been shown to happen around this area



[31]. From 200 °C to 340 °C the mass loss is attributed to the decomposition of F127. This decomposition is reported to continue until 580 °C in [32], but at 340 °C the PVP in the membrane also starts decomposing very fast until 480 °C. From there, a slow decomposition of residual PVP and F127 is believed to happen.

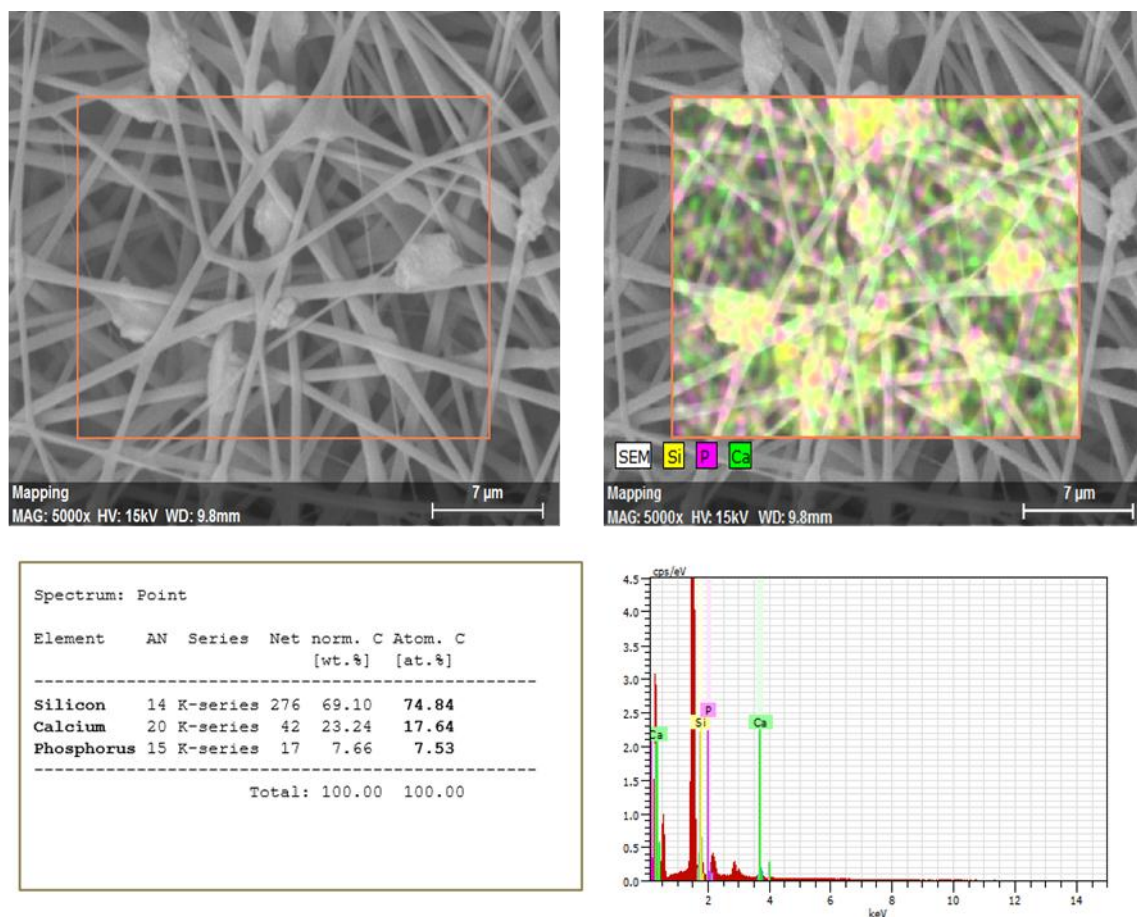


Figure 4.8. SEM image of the PVP 14 wt.% and BAG 14 wt.% membrane (top, left), and the respective EDS elemental map (top, right). Normal and atomic Concentration (wt.% and at.%) quantification on the left down image. Element spectrum on the right down image (carbon and oxygen were ignored) (see Figure 6.2 in supplementary information for complete information of the element colour trace).

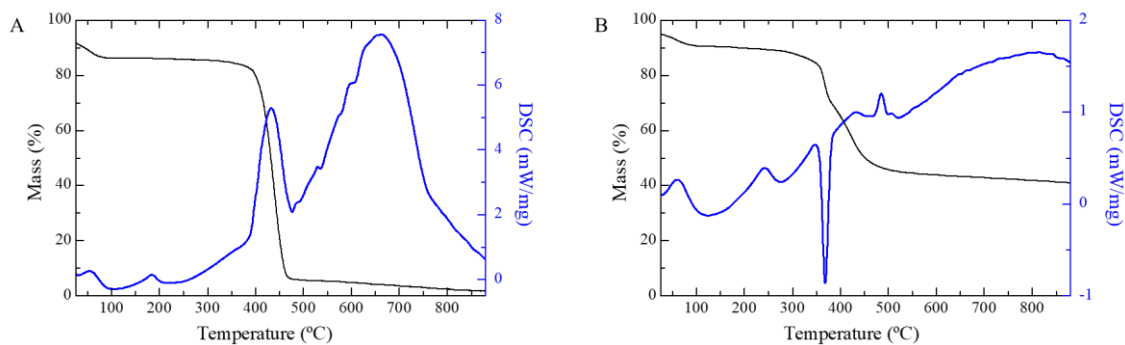


Figure 4.9. DSC/TGA of plain PVP membrane (A) and of composite PVP 14 wt.% and BAG 14 wt.% membrane.

From this analysis, it is possible to determine the PVP crosslinking temperature which is around 190 °C for plain PVP membranes and a little bit higher for PVP+BAG membranes. Also, PVP and F127 components can be eliminated (if wanted) with temperatures around 500 °C.

#### 4.2.2 Composite membranes of PVP, BAG and IONPs

Previously synthesized IONPs were incorporated in the electrospinning solution by adding a known concentration to the PVP 14 wt.% BAG 14 wt.% solution in a concentration of 4 wt.% relative to the PVP mass. This solution was mixed by mechanical stirring for about 20 min. The following solution was electrospun with 20 kV; 20 cm; 0,15 ml/h with 35% relative humidity and 25 °C.

The same analysis process was applied on the electrospun PVP/BAG/IONPs membrane. In Figure 4.10 a sample of the composite membrane was observed in SEM and EDS. The addition of IONPs seems to not influence the morphology of the fibres (Top, left). The EDS elemental map (top, middle) shows the presence of BAG components (Si, Ca, P) but also the clear presence of iron (top, right) from the IONPs added. The quantification of normal and atomic concentration (bottom left) is merely indicative of the presence of iron and does not translate to the overall normal and atomic concentration of the membrane. The small size of NPs (around 10 nm) makes it impossible to observe with this SEM equipment. Transmission Electron microscopy (TEM) analysis would be more suitable to observe the IONPs.

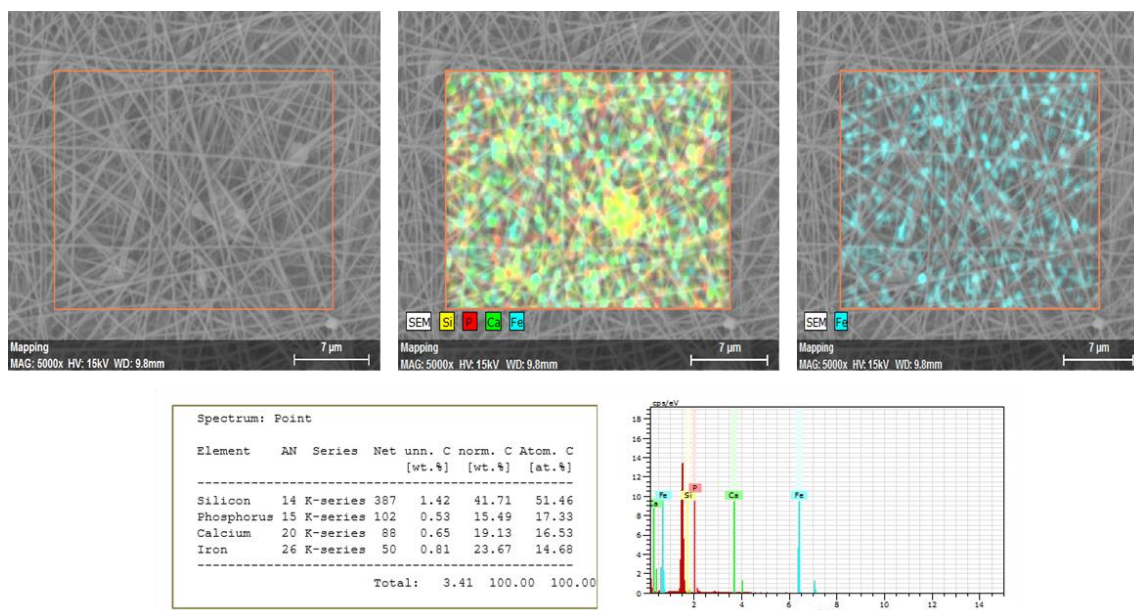


Figure 4.10. SEM image of the PVP 14 wt.%, BAG 14 wt.% and 4% IONPs membrane (top, left), and the respective EDS elemental map. Normal and atomic Concentration (wt.% and at.%) quantification on the left down image. Element spectrum on the right down image (carbon and oxygen were ignored) (see Figure 6.3 in supplementary information for complete information of the element colour trace).

#### 4.2.3 Thermal and UV crosslinking of PVP membranes

PVP is soluble in aqueous solutions, and consequently it is unsuitable for biomedical applications. To make PVP water-insoluble membranes, the polymer must be crosslinked. PVP crosslinking has been successfully reported by thermal treatment [31] and by UV treatment [33], with both stimulus enabling different polymer chains to link through a covalent or ionic bond, promoting changes in the polymer physical properties.

For the UV crosslinking, a UV light was used. Plain PVP 18 wt.% membranes were submitted to different UV times: 30 min, 1, 2, 3, 4, 5 h. The samples were then immersed in water with an immediate change of white colour membrane to a transparent film (Figure 4.11). This indicates that the fibrous structure of the membrane was lost and that after UV crosslinking the membranes were still water-soluble.

However, from Figure 4.11 it is not clear what happens to the membrane structure after immersion, so samples (after immersed) were analysed on SEM (Figure 4.12) to study the structure of the membrane with the UV crosslinking time. With the SEM analysis we see that samples with increased UV exposure have more tendency to completely lose their desired fibrous structure, turning it into a film. Already with 30 min and 1 h, the differences are clear and with 2 h UV it is no longer possible to observe any fibrous structure.



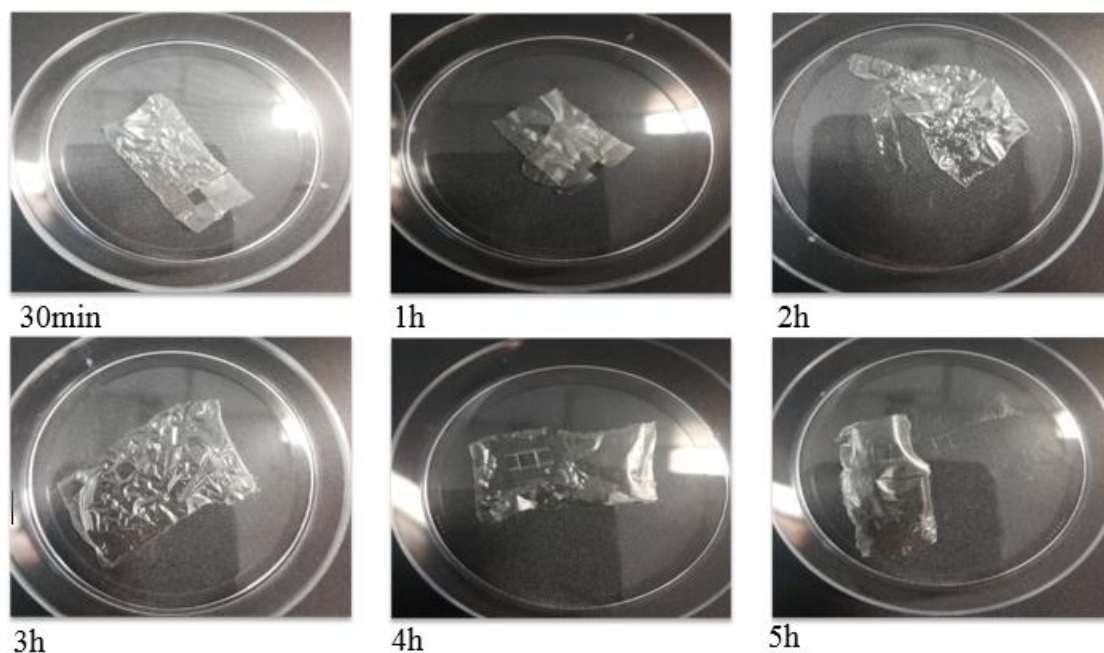


Figure 4.11. Plain PVP 18 wt.% membranes with different UV crosslinking times after immersed in water.

As for the thermal crosslinking, samples were initially crosslinked with temperatures of 200 °C and 175 °C and 1.5 and 10 h. However, the temperature control was difficult, and samples were scorched (turned into dark brown) and fibres lost their morphology and structure. The temperature was decreased to 150 °C for 5, 10, 15, 20 and 24 h. With this treatment conditions the membrane was not scorched and when immersed in water, did not dissolve. Through SEM analysis, the structure and morphology of the fibres were evaluated. Figure 4.13 shows SEM images of plain PVP membranes after thermal crosslinking. Comparing a plain PVP membrane before and after crosslinking at 150 °C at different times after immersion, confirms the maintenance of the fibrous structure for times above 20 h. At 5 h, the structure is practically fully destroyed, while after 10 h it starts getting possible to see a fibrous look alike structure. After 15 h a fibrous structure is maintained but the fibres are still affected by the water absorption. After 20 h and 24 h the differences are very small, and a fibrous structure is fully maintained.

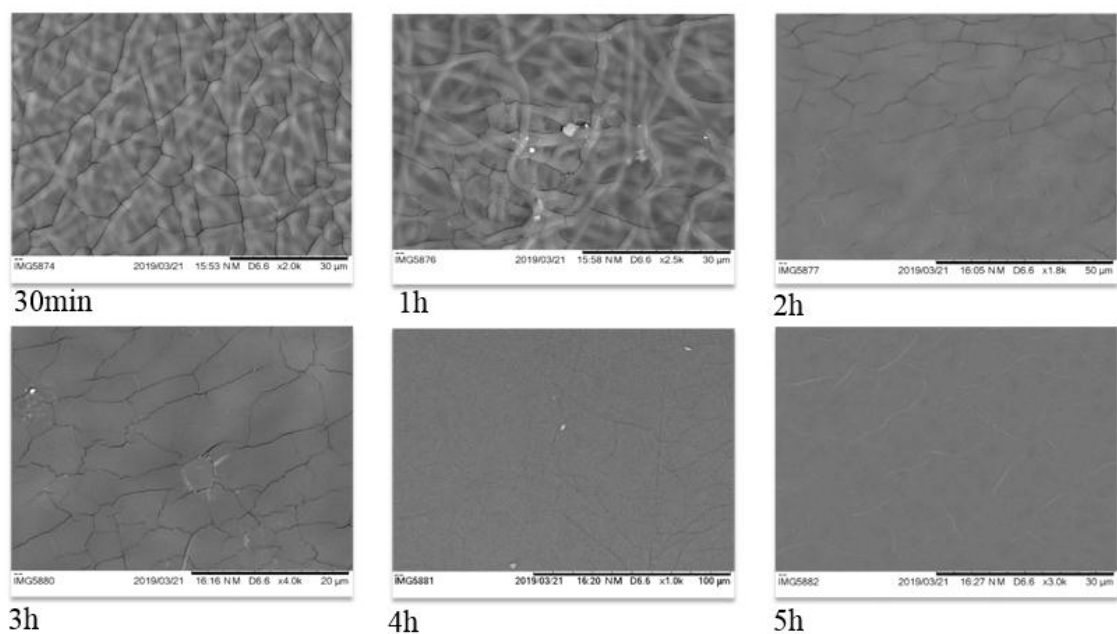


Figure 4.12. SEM analysis of the respective PVP 18 wt.% membranes with different UV times in Figure 4.11 after immersed in water.

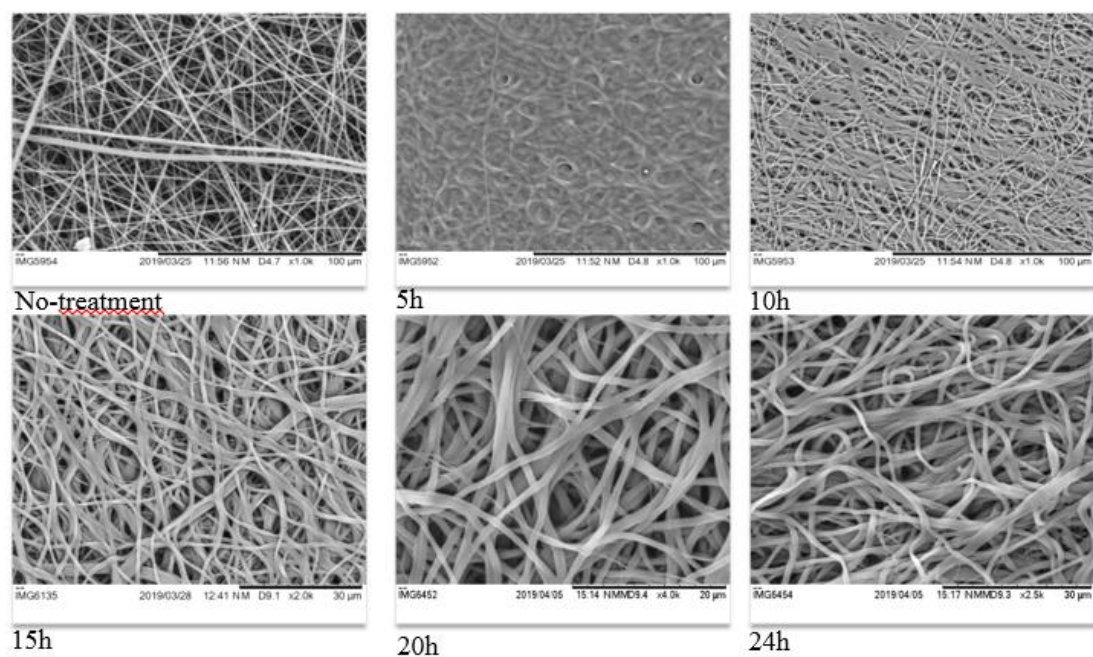


Figure 4.13. PVP membrane without treatment before immersion, and PVP membranes with thermal cross-linking of 150°C with different cross-linking times, after immersion (note: To be able to properly observe the structure different magnifications had to be used for each sample, therefore the magnification used should not be considered).

Based on these results, composite membranes were crosslinked at 150 °C for 24 h. Figure 4.14 shows SEM images of plain PVP, PVP/BAG and PVP/BAG/IONPs membranes before and after thermal crosslinking. The crosslinked membranes were immersed in ultra-pure water to test their solubility, and unlike the non-crosslinked membranes, they did not dissolve instantly. They were then immersed in water for 24 h and dried at 40 °C. In Figure 4.14, we can see their microstructure through SEM images. Comparing these images with the respective membranes before immersion in water, we can observe some swelling of the fibres. This swelling change the fibres morphology and dimension which might change the membranes bioactivity and mechanical properties, as they are directly influenced by the surface area and consequently the diameter and shape of the fibres. This swelling capacity should be quantified by measuring the amount of water that the membrane can absorb in an established period of time. Also, with this analysis it is not clear if the membranes are fully water insoluble. The membranes seem to not dissolve in the naked eye, but there is the possibility that some part of the membrane is lost to the solvent. A study measuring the mass of the solvent and of the membrane before and after immersion should provide this information about the membrane properties.

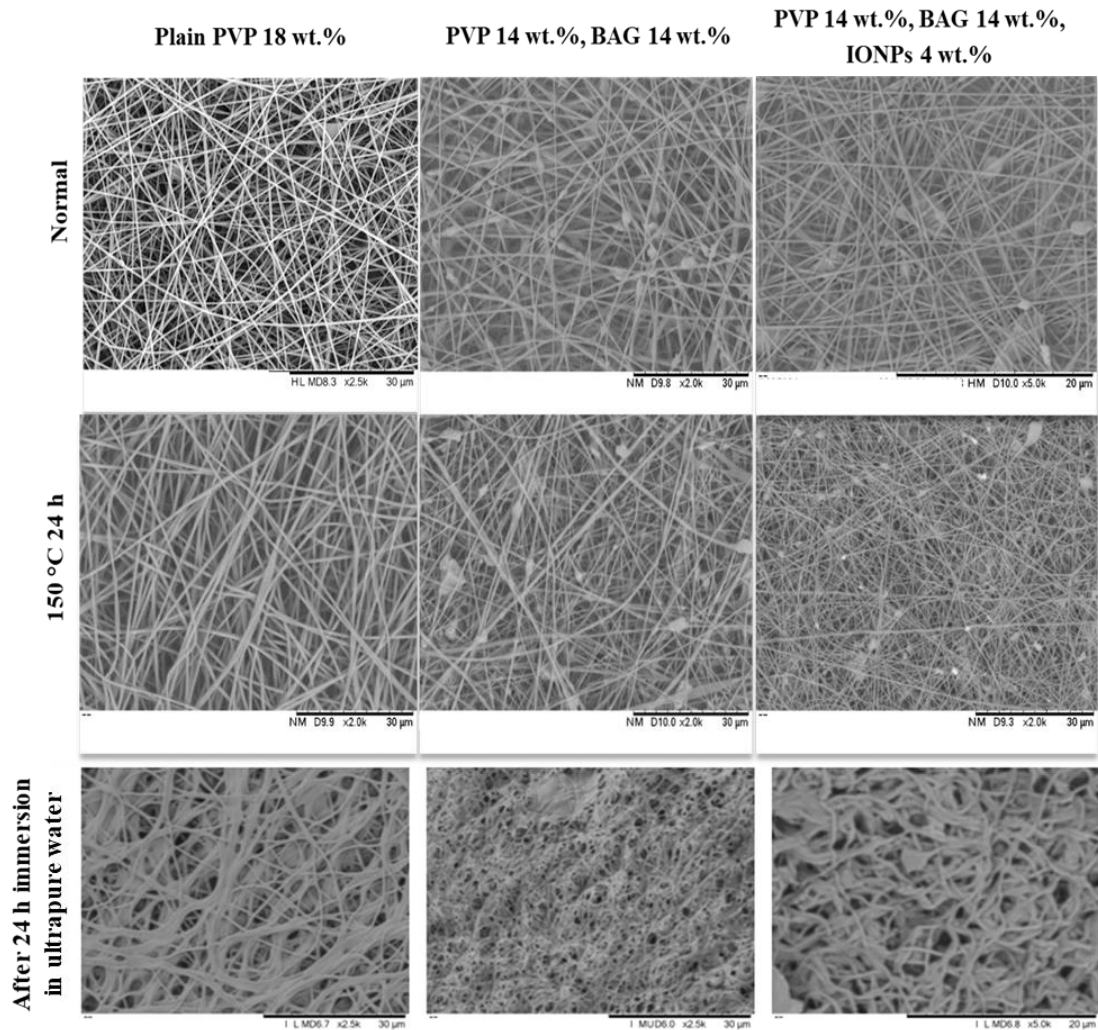


Figure 4.14. PVP, PVP BG, PVP BG IONP's membranes observed on SEM, before and after crosslinking at 150 °C for 24 h, and after 24 h immersion in ultra-pure water and drying.

### 4.3 Magnetic hyperthermia Assays

Magnetic hyperthermia assays were performed to evaluate the heating capacity of the IONPs alone and IONPs in the PVP/BAG membranes, in the presence of an alternating magnetic field. All assays were performed during 10 minutes with a magnetic flux density of 300 Gauss and a frequency of 418.5 kHz. Figure 4.15 represents the temperature variation for assays on a 1 ml aqueous solution with 4% IONPs. Three assays were performed, giving an average temperature variation of  $22\text{ }^{\circ}\text{C} \pm 1.8^{\circ}\text{C}$ . Samples of 10 and 20 mg of a PVP/BAG/IONPs composite membrane were tested (Figure 4.15). The concentration of IONPs in the membrane (4% of the polymer mass) is lower than in the aqueous solution (4% of the solution), therefore lesser NPs are present on the membrane samples, therefore lower temperature variation were expected as confirmed with average temperature variations of  $0.7 \pm 0.15\text{ }^{\circ}\text{C}$  for 10 mg of membrane and  $2 \pm 0.36\text{ }^{\circ}\text{C}$  for 20 mg of membranes.

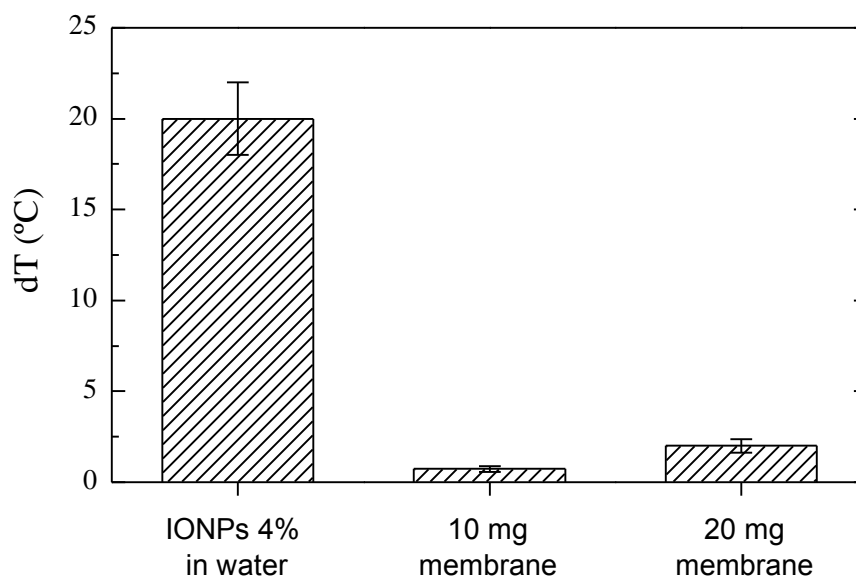


Figure 4.15. Temperature variation ( $^{\circ}\text{C}$ ) from magnetic hyperthermia assays for IONPs in 4% aqueous solution, 10 and 20 mg of 14 wt.% PVP, 14 wt.% BAG, and 4 wt.% IONPs.

The increase of heating capacity ( $1.3\text{ }^{\circ}\text{C}$ ) with the double of membrane mass (and consequently double IONPs) is also stated. If the normal body temperature is considered to be  $37^{\circ}\text{C}$ , a temperature variation of  $0.7\text{ }^{\circ}\text{C}$  (10 mg membrane) and  $2\text{ }^{\circ}\text{C}$  (20 mg membrane) would not be enough to reach the desired therapeutic temperature for magnetic hyperthermia on cancer tissue (between  $40$  and  $44\text{ }^{\circ}\text{C}$ ), without more membrane mass or IONPs concentration. Nevertheless, the incorporation of IONPs in a polymeric bioactive glass membrane was successful and added a new property (potentially useful for magnetic hyperthermia treatment) to the membrane.

### 4.4 Bioactivity Assays in SBF

The bioactivity assays are performed on materials as a reference for further evaluating *in vivo* bioactivity using animals or other sources. The thickness, coverage, form of apatite and time

taken to deposit apatite are often estimated. Figure 4.16 shows the evaluation of a PVP 14 wt.% and BAG 14 wt.% composite membrane in different immersion times on SBF. BAG particles observed in non-immersed membrane are thought to start forming apatite, as this is the BAG purpose in the composite. However, with increasing immersion times it is not possible to observe these particles anymore. From 6 to 12 h we can observe a slight difference where a film starts forming after 12 h immersion in SBF. This film formation may be due to the apatite formation and after 24 h this effect is aggravated; however, this is not coherent in the following images.

To further analyse the formation of apatite on the membrane, FTIR and DRX analysis should be used to chemically confirm the apatite formation. The soluble species of silica, phosphate and calcium concentrations in SBF before and after immersing the membrane should also be measured to assess the SBF uptake of the species. This measurement could give a more precise estimative of the time taken by the membrane to dissolve each of the species and consequently the time taken to form apatite on the membranes.

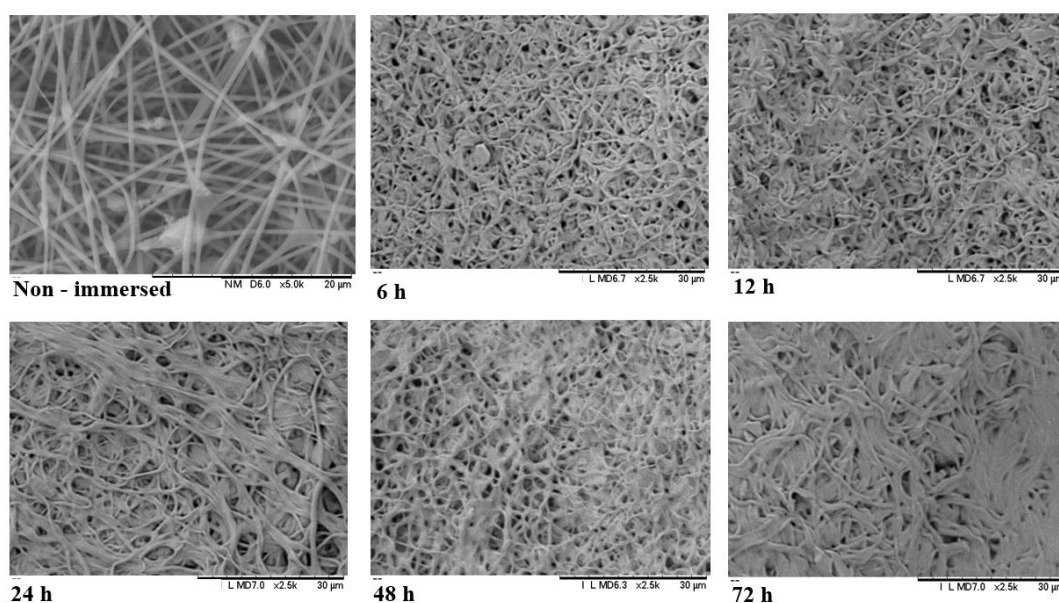


Figure 4.16. SEM images of the PVP 14 wt.% and BAG 14 wt.% after 6, 12, 24, 48 and 72 h immersion in SBF.

## 4.5 Cytotoxicity Assays

In order to ascertain the biocompatibility of the PVP membranes with BAG and IONPs, the potential cytotoxic effect of these membranes on Vero cells was evaluated using the extract method (ISO standard 10993-5). The results are shown in Figure 4.17 which expresses cell viability in %. The cell viability (%) was determined following the procedure in supplementary information. The assays were performed for an extract concentration of 16 mg/ml with an uncertainty of 5 %. Two dilutions (factor 2) were performed for each membrane and 5 replicas for each sample. The control medium shows a cell viability around 100% and was used as reference for the following samples. All pure PVP samples revealed no cytotoxicity with cell viability (%) of 92 % (for normal concentration) and 96 % (for dilution 1) and 91 % (for dilution 2), proving the expected biocompatibility of the PVP.



The BAG (14 wt.% PVP, 14 wt.% BAG membrane) revealed to be moderately cytotoxic for the cells with  $72 \pm 6$  % cell viability. Following dilutions BAG D1 and BAG D2 proved to increase cell viability to  $81 \pm 2$  % and  $87 \pm 3$  %. Although both values are labelled as slightly cytotoxic, D2 is very close to being considered non cytotoxic. Thus, given the biocompatibility of PVP, the cytotoxicity of these samples is dependent on BAG presence. The fact that both dilutions increased cell viability suggests that the concentration of BAG can be tuned to show no cytotoxicity.

IONPs membrane (14 wt.% PVP, 14 wt.% BAG, 4 wt.% IONPs) also showed a moderately cytotoxic behaviour for the Vero cells with  $78 \pm 4$  % cell viability. Dilution 1 improved for  $81 \pm 5$  % (slight cytotoxic) and Dilution 2 increased to  $88 \pm 5$  % and can be considered non cytotoxic. These results are similar to the BAG membrane, which might suggest that this particular IONPs concentration has no effect on the cell viability. A study carried out by the research group has proven possible to produce non-cytotoxic membranes with these NPs [4], which again points to the cytotoxicity of BAG.

The pH of BAG membrane extract concentration was tested with a colorimetric test on site and it confirmed an alkaline pH. It is possible that the alkyne nature of BAG present in the membranes may have affected the cells proliferation, during the test. To confirm this, BAG pH should be controlled during synthesis and placed in a dialysis process until it turns neutral and the cytotoxicity assays should be repeated in the same conditions.

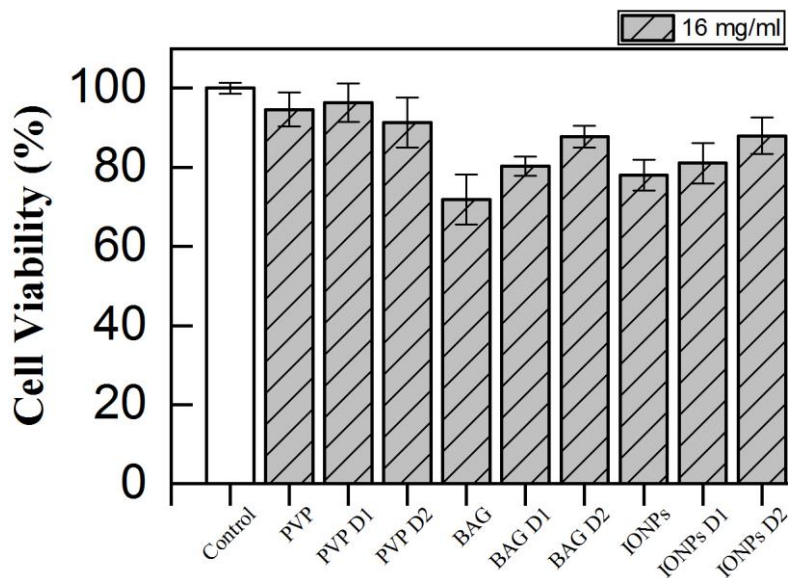


Figure 4.17. Vero cell viability (%) after indirect exposure to the different electrospun membranes. PVP corresponds to plain PVP 18 wt.% membrane; BAG corresponds to composite PVP 14 wt.% and BAG 14 wt.% membrane; and IONPs correspond to composite PVP 14 wt.%, BAG 14 wt.% and IONPs 4 wt.% and respective dilutions 1 and 2 (factor 2).



## 5 Conclusions and future perspectives

This work had as its central objective the production and characterization of a composite membrane of non-sintered BAG, IONPs and biodegradable PVP by the electrospinning technique, and respective process optimization, so that they can be used in cancer therapy through magnetic hyperthermia and bone regeneration.

Producing a non-sintered BAG represents an advantage in terms energetic costs as it does not require high temperatures. However, the presence of the structural agent may originate some problems in properly characterizing this material, as the presence of F127 was found to possibly mask some characteristics of the silica, calcium and phosphate species. This made it hard to fully understand of the phenomenon reported in this work.

SEM analysis of the fibres showed the effects of the different parameters (flow rate, applied voltage, needle-collector distance and humidity) on the morphology and average size of the fibres of PVP BAG composite membrane. After experimenting low BAG concentrations within the polymeric solution and reducing the BAG particle size it was shown that the BAG concentration could be augmented up to a 14 wt.% concentration, and it is thought to be possible to increase this concentration even more, while adjusting the polymer concentration. After selecting the lowest average fibre sizes and the most practical parameters, 20 kV, 20 cm, 0, 15 ml/h and humidity % levels around 30–40 % were selected to produce PVP 14 wt.% and BAG 14 wt.% membranes. As IONPs were easily incorporated in the membrane without changing the solution viscosity, the same parameters were used for the PVP BAG IONP's membranes.

A study regarding the membranes crosslinking was performed by testing two different crosslinking processes. UV cross-linking did not show any signs of properly reticulating the membrane and was quickly abandoned. Thermal crosslinking on the other hand proved to be a suitable process, as a 150 °C for 24 h treatment proved to turn the membranes into water-insoluble materials.

Through magnetic hyperthermia assays, the membranes with IONPs revealed the (small) ability to generate heat under an alternative magnetic field stimulus and confirmed the successful incorporation of the IONPs in the membrane without the IONPs losing their super paramagnetic properties. The quantity of IONPs was shown to influence the hyperthermia performance and with further studies, can be tuned to generate enough proper heat for clinical applications.

The bioactivity assays were inconclusive as the process variants and components must be much more supervised. It seems that there is an ionic exchange between the membrane and SBF, but further analysis must be performed to confirm this.

Regarding the cytotoxicity assays, BAG concentration proved to add some cytotoxicity to this system. Only with a second dilution from the original extract concentration, was possible to obtain a non-cytotoxic sample. This cytotoxicity from the BAG was attributed to its alkaline pH, which means that a dialysis step must be added to the BAG synthesis.

Overall, it was possible to produce a composite membrane as intended and which can serve as support for a more efficient delivery of NPs, but although the membranes showed some potential regarding magnetic hyperthermia, they seemingly lacked the also desired bioactive properties.



A low bioactive performance was expected, as neither the BAG nor the fibres themselves have micro or Nano porosity, which is a very crucial property for this matter, but the analysis were not conclusive and not promising at all, as we conclude that the exploration of new alternatives should be prioritized to the detriment of the alternative presented here in this work.

## 5.1 Future Perspectives

Like is was stated above, this work was performed in parallel with a PhD student and some of the studies here presented may give some information regarding the production of a composite with the same intended characteristics.

Regarding magnetic hyperthermia treatment, it is important to understand the heat generating mechanisms of the IONPs as they generate heat from the Néel relaxation (rotation of the nanoparticle internal dipole) and Brownian relaxation (physical rotation of the nanoparticle). In the membrane it is possible that the Brownian relaxation does not occur, because the IONPs are trapped and therefore the hyperthermia performance of the IONPs in the membrane will not match free IONPs. It would be important to study the variation of the hyperthermia performance, of an immersed membrane, with the time. If the IONPs escape from the membrane into the solution, the Brownian relaxation will return and count to the hyperthermia effect.

New incorporation methods should also be tested. A more efficient incorporation means a higher amount of IONPs in the membrane and a better control of the hyperthermia effect.

Regarding the BAG, as referred above the micro and nano porosity are crucial to the high bioactivity and cell attachment performance, therefore ensure these properties is a must in future studies, whether by calcination of the BAG during the synthesis, or by calcination of the fibrous membrane with the BAG inside. In this last strategy, a higher BAG concentration may be required, because if the membrane is majorly composed by a polymer, the polymer will be removed during the calcination process and only the BAG will remain.

The membranes should also be mechanically characterized. For surgical implantation the membranes need to malleable and resistant, therefore studying and improving these properties is also very important.

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## 6 Supporting information

### 6.1 Tested electrospinning parameters

Table 6.1. Electrospinning parameters tested using different concentrations of BAG in an 18 wt.% PVP solution in ethanol.

Sample	BAG wt. %	Flow Rate (ml/h)	Applied Voltage (KV)	Needle-collector distance (cm)	Humidity %	Temperature (°C)
A1	1	0,2	15	15	24	25
A2			20	20	27	
A3			15	15	24	
A4			20	20	24	
A5		0,4	15	15	24	
A6			20	20	25	
A7			15	15	24	
A8			20	20	28	
B1	2	0,2	15	15	24	25
B2			20	20	28	
B3			15	15	25	
B4			20	20	28	
B5		0,4	15	15	24	
B6			20	20	24	
B7			15	15	24	
B8			20	20	24	
C1	3	0,2	15	15	30	25
C2			20	20	30	
C3			15	15	30	
C4			20	20	30	
C5		0,4	15	15	30	
C6			20	20	30	
C7			15	15	28	
C8			20	20	30	
D1	4	0,2	15	15	30	25
D2			20	20	30	
D3			15	15	29	
D4			20	20	30	
D5		0,4	15	15	29	
D6			20	20	30	
D7			15	15	30	
D8			20	20	29	

E1			15	15	30	
E2		0,2	15	20	29	
E3			20	15	30	
E4	5		20	20	30	25
E5			15	15	30	
E6		0,4	15	20	30	
E7			20	15	30	
E8			20	20	30	

Table 6.2. Set of electrospinning parameters tested using a solution of 14 wt.% PVP and 14 wt.% BAG (both relative to solvent mass) in a mixture of ethanol:water in a ratio of 85:15 (v/v).

Sample Number	Flow Rate (ml/h)	Voltage Applied (kV)	Needle-Collector Distance (cm)	Humidity
1	0,05	15	15	38
2			18	
3			20	
4		18,3	15	
5			18	
6			20	
7		20	15	
8			18	
9			20	
10	0,15	15	15	37
11			18	
12			20	
13		18,3	15	
14			18	
15			20	
16		20	15	
17			18	
18			20	
19	0,25	15	15	35
20			18	
21			20	
22		18,3	15	
23			18	
24			20	
25		20	15	
26			18	
27			20	

## 6.2 Procedure for *in vitro* cytotoxicity evaluation

The cytotoxicity study was performed using the extract method which consists of placing the cells in contact with the medium where the membranes were previously incubated. To determine the number of viable cells, a colorimetric method based on the resazurin reagent was used, which is reduced by the living cells. For the extract production, different samples of 40 mg  $\pm$  5% were pre-sterilized with UV irradiation for 1 hour. Subsequently, each membrane was placed in 2.5 ml of medium, at 37 °C, for 48 hours. Cells were seeded into 96-well plates (Figure 6.1) and 15 wells were used for each type of membrane (45 wells total: 5 replicas for the initial concentration of extract medium 16 mg/ml and 5 replicas for each of 2 dilutions of factor 2 from the initial concentration). In addition, negative (column 1, 5 replicas), positive (column 11, 3 replicas) and cell-mediated controls (column 1, 3 replicas) were performed, serving as reference for calculating cell viability.

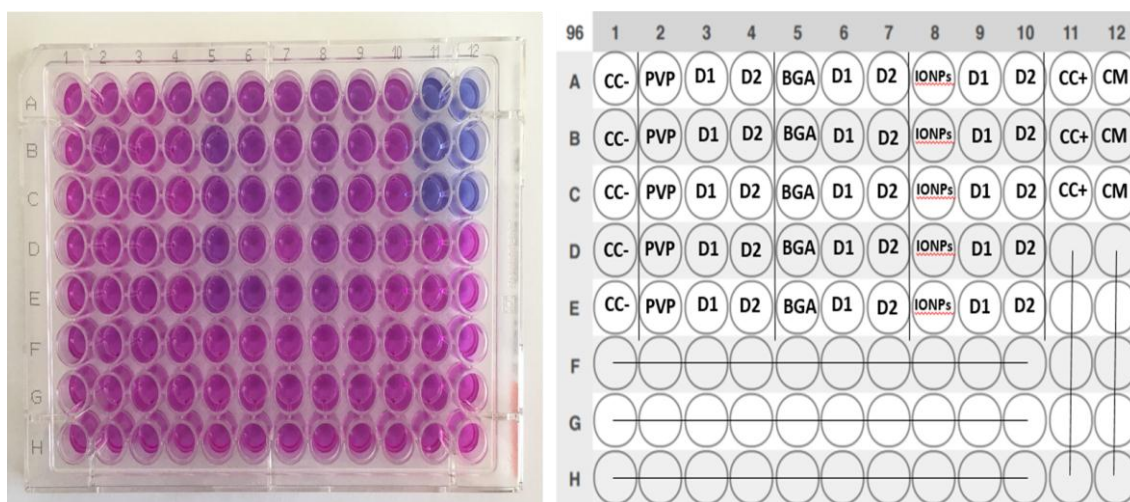


Figure 6.1. Schematic planning for cytotoxicity assays.

The plate was again placed in the incubator for 48 h. Resazurin was used for cell viability analysis. After 48 hours in the incubator, the plate was removed and as well as the medium contained in each well. A solution of 90% of medium and 10% resazurin was then placed in each well. The viability analysis consists of a change in the colour of the solution (a pink colour means live cells and a blue colour means the presence of dead cells). The plate was placed in the incubator for 4 hours. After this time, the absorbances of each well (at 570 nm and 600 nm) were measured in a Biotek ELX800 microplate reader. To determine the cell viability %, medium control and uncertainties, the means of each 5 replicates were calculated for each sample and the following expressions were used:

$$\text{Medium Control} = \text{"Average } i\text{"} - \text{"Average } CM\text{"}$$

$$\text{Cell Viability} = \frac{\text{"Average control"}}{\text{"Average C-"} - \text{"Average } CM\text{"}}$$

$$\text{Uncertainty} = \sqrt{\sigma^2 + \sigma_{CM}^2}$$

Where  $\sigma$  represents the standard deviation for each of the concentrations used and  $\sigma_{CM}$  is the standard deviation of the control medium. In order to analyse cell viability, it is necessary to take into account four denominations according to the percentage of viability obtained and they are: viability greater than 90 % the material is non-cytotoxic; with cell viability between 80% and 89 % considered to be slightly cytotoxic; between 50 % and 79 % is moderately cytotoxic; if it is less than 50 % is severely cytotoxic.

### 6.3 SEM/EDS elements colour trace of composite membranes (PVP/BAG)

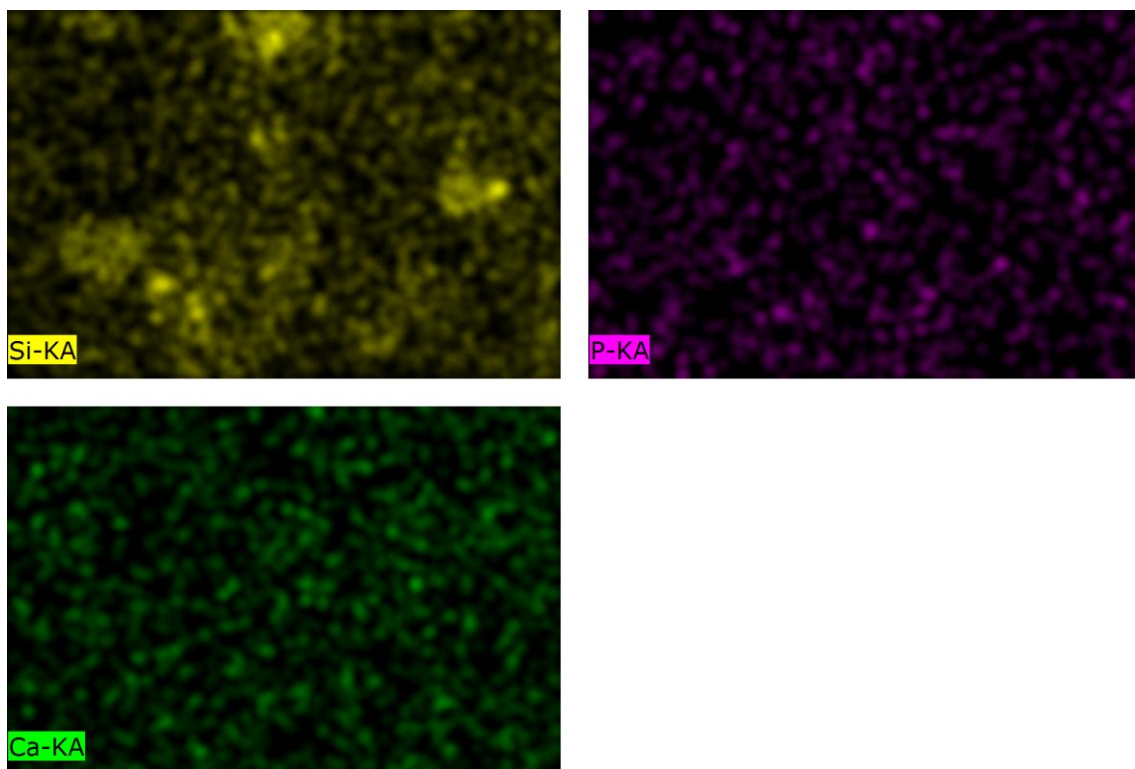


Figure 6.2. SEM/EDS elements colour trace attached to Figure 4.8.

#### 6.4 SEM/EDS elements colour trace of composite membranes (PVP/BAG/IONPs)

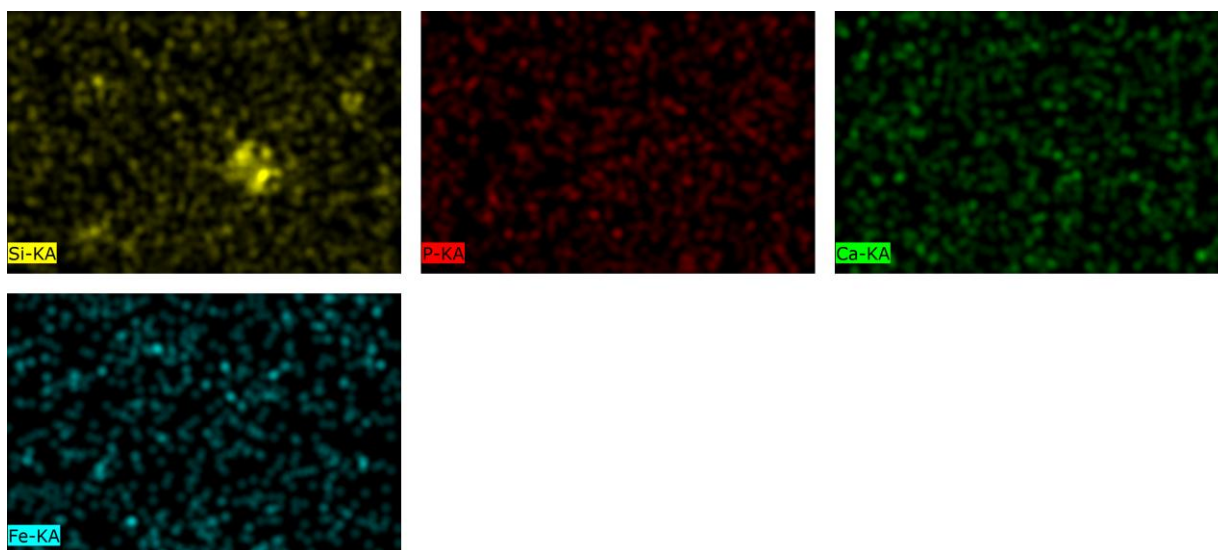


Figure 6.3. SEM/EDS elements colour trace attached to Figure 4.10.