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THE CATALYTIC VAPOR PHASE BUTTLATION OF PHENOL

By

Nathan Lewis Zutty

A thesis presented to the Department of Chemistry of Union College in partial fulfillment for the degree of Bachelor of Science with a Major in Chemistry.

Mathan L. Soly

approved by Howard E. Sheffer

June, 1954

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Acimowledgment

To Doctor Howard E. Sheffer, Whose helpful guidance made this thesis possible.

SEPT, 9, 1954

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Introduction

The purpose of this experiment is to study the reaction between secondary butyl alcohol and phenol in the vapor phase. The effect of temperature upon the formation of different butyl phenols and butyl phenyl ethers was observed.

Historical

+ 1

The principle products of the reaction between an alkyl alcohol and phenol over an activated alumina catalyst consist of mono-substituted alkyl phenols, alkyl phenyl ethers, and higher boiling fractions, consisting of polysubstituted alkyl phenols and ethers.

The mechanism of this reaction has not been conclusively proven, however it is supposed that all of the reaction products result from the rearrangement of an alkyl phenyl ether. This is in accordance with the activated complex theory of Eyring 12. and may come about in this way:

or more simply:

where the reacting molecules arrange themselves for reaction
by means of a catalyst thru hydrogen bonding. From this
phenyl ether the reaction can supposedly go in two ways:
First by an intramolecular rearrangement where the alkyl group
shifts to the ring and secondly., by an intermolecular rearrangement where the alkyl group
ment where the alkyl group of the ether reacts with another
phenyl nucleus to give substituted alkyl phenols. The latter
proposal has gained wider acceptance. It may be explained
by the following reactions:

Where R is CH_CH_C -CH_

Perry 13. reports that increasing the temperature of the reaction results in an increase in alkyl phenols and a decrease in phenolic ethers. This would be in support of the intermolecular rearrangement theory. Quite a bit is known about the

rearrangement of alkyl phenyl ethers. Claisen 14. found that allyl phenyl ethers rearrange intramolecularly to allyl phenols. But Smith 15. also noticed that iso, secondary, and tertiary butyl phenyl ethers rearrange all giving the same p-tert. butyl phenol when aluminum chloride is used as a rearranging agent. This indicates that the reaction is intermolecular inspead of intramolecular as Claisen 14. supposed.

A third possibility was proposed by Sprung and Wallis 18, who said that elkyl phenols are not formed by an intramolecular rearrangement, but are produced by result of a reaction between two molecules of an ether. They prepared various butyl phenyl ethers in optically active forms and studied their rearrangements under various conditions. In each case the alkyl phenols formed retained their optical activity. The intermolecular rearrangement ment proposed by Sprung and Wallis is:

This type of reaction explains the presence of olefins in the catalytic vapor phase alkylation of phenol; and moreover the presence of poly-substituted phenols which are also formed.

Experimental

A diagram of the apparatus used in the reaction run appears in figure one. The phenol-sec, butyl alcohol feed is introduced into the reaction chember by means of nitrogen pressure upon its surface. The pressure and hance the drop rate is controlled by means of a glycol pressure regulator which works by lowering or raising the center tube. The feed solution, in a 1:1 molar ratio, passes up thru a capillary tube and then drops into the reaction chamber. The drop rate can be observed in the glass tube which leads into the heated catalyst chamber. The reactants drop into a heated stainless steel tube, 3.5 feet long (figure two) , vaporize and pass thru the catalyst chamber. They condense in the lower section of the tube, and are collected in a Grignard flashat the bottom. The reaction chamber was divided into three parts all heated and carefully controlled by means of two variacs and a rhoostat. The temperature measured by meands of a chromel alumel thermocouple which is placed at intervals along the reaction chamber in a tube concentric with it. The E.M.F. developed by this system is measured by a Leeds-Northrup potentiometer set up. The temperature may be controlled separately in either of the three sections by the voltage control apparatus which are connected to the heaters. Thirty-two grams of activated alumina catalyst are used for a six hour

run, this fills the catalyst bed to a depth of four inches and results in a contact time of approximately 3.5 seconds. 515 milliliters of feed were used for the run at an average temperature of 287° centigrade. The temperature is measured at one inch intervals along the reaction tube and then everaged to find the temperature of the run. The gases formed during the reaction, including the nitrogen used to control the drop rate were collected in a twenty liter bottle for later analysis.

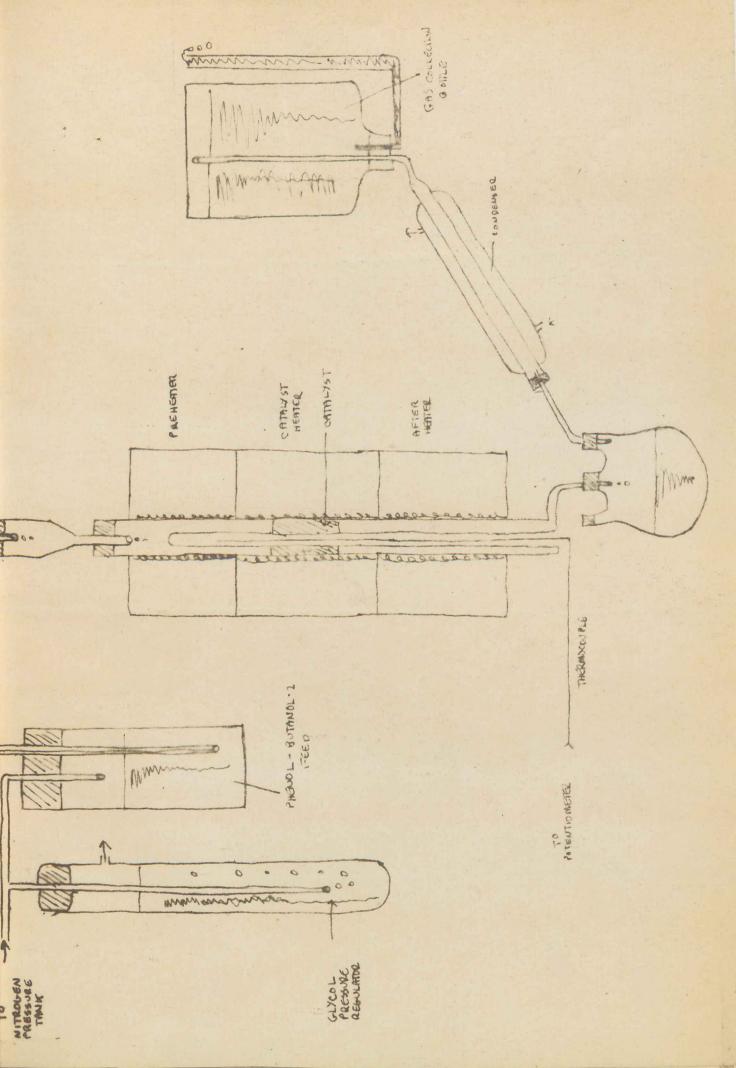
Separation of Butylphenols from Phenolic Ethers (13)

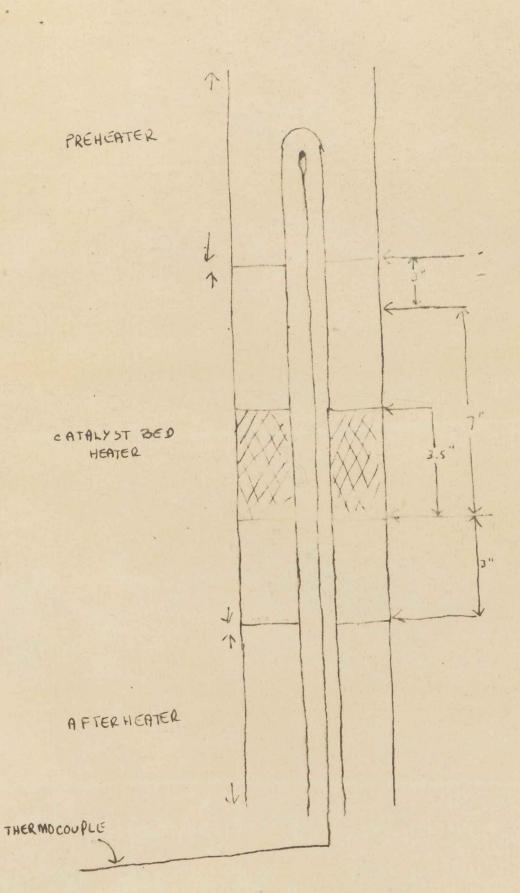
The crude product is treated with 600cc. of 20% sodium bydroxide. The two layers are separated and the alkaline layer is then washed four separate times with 50cc. of ethyl ether to remove any remaining phenolic ethers. These extractions are then combined with the original phenolic ether layer.

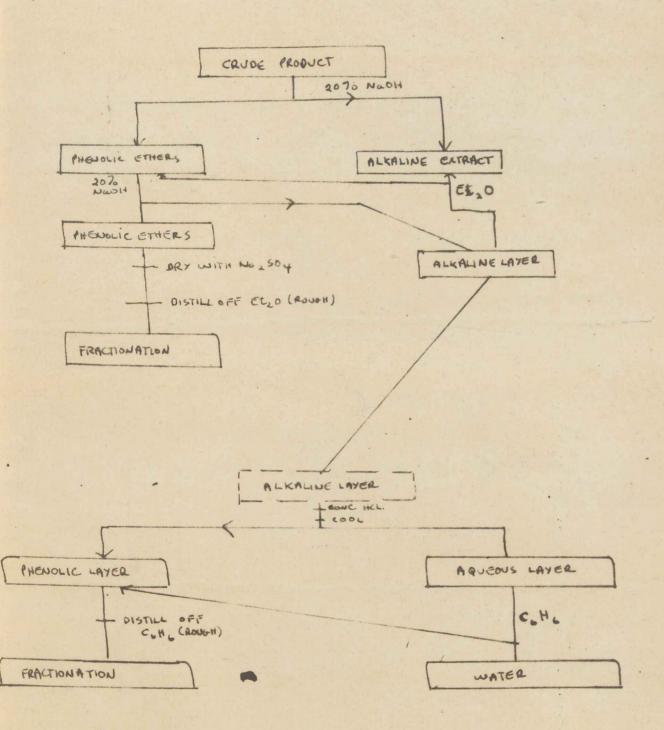
The phenolic ethers are now treated with 50cc. of 20% sodium hydroxide. These extracts are combined with the original alkaline layer.

The phenolic ethers are now dried with enhydrous sodium sulfate. The alkaline layer is now acidified with concentrated hydrochloric acid (250cc.). After cooling the phenolic and equeous layers are separated. The equeous layer as washed four times with 50cc. of benzene each time.

The ethyl ether and benzene are roughly distilled from the ether and phenolic layers respectively, and the two are ready for fractional distillation.







Distillation of Phenols

ethers they are fractionally distilled. A column of thirty theoretical plates is used (figure four). It is approximately four feet tall and one-half inch in diameter and is packed with 5/32 of an inch stainless steel helices. For fractionation a reflux ratio of 15:1 is used; this means that for every fifteen drops condensing at the top of the column, one is withdrawn. The column is insulated by an outer shell of diatomaceous earth. The column and stillpot are heated by means of variace. Good control is obtained this way.

As the products distilling are high boiling and melting the outlet from the condenser was heated by an infra-red heat lamp to prevent clogging.

An inert chaser, diphenylamine, he added to the stillpot to insure complete fractionation.

Graphs and the data of this run are found in the appendix.

Distillation of Phenolic Ethers

The ethers contain water and must be azeotropically distilled with benzene to insure complete drying as the sodium sulfate was not effective. If this is not done the phenolic ethers form a constant boiling mixture with their water and fractionation could not be attempted.

Since the amount of ethers formed are small, a small

three bubble Snyder column is used. This corresponds to three theoretical plates and has no hold up. (figure 5)
The column is wrapped in asbestos paper since the others are very high boiling. A good separation is obtained.

Graphs and data of this distillation appear in the appendix.

Butyleno Ces Analysis

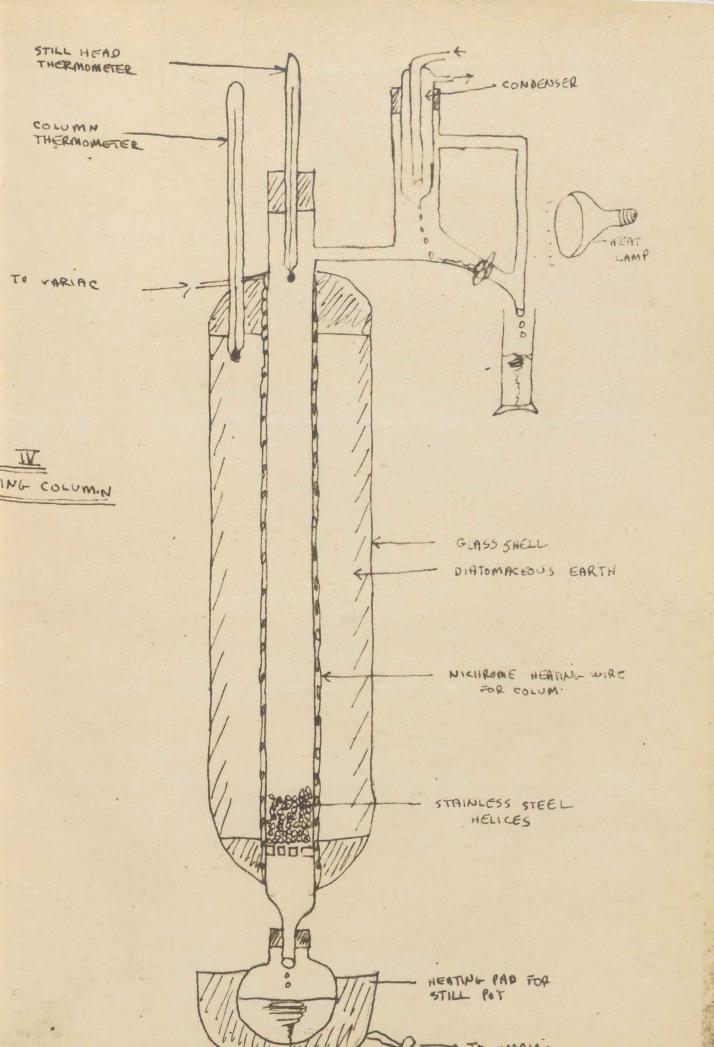
The gas produced during is assumed to consist of butylenes. Since it comes over mixed with nitrogen, it was found necessary adsorb the gas in a solution of browine in carbon tetrachloride to rid it of its nitrogen. The nitrogen is collected in a large bottle and the amount of butylenes produced are found by subtraction. The gas was passed thru the adsorbant twice to incure complete adsorption.

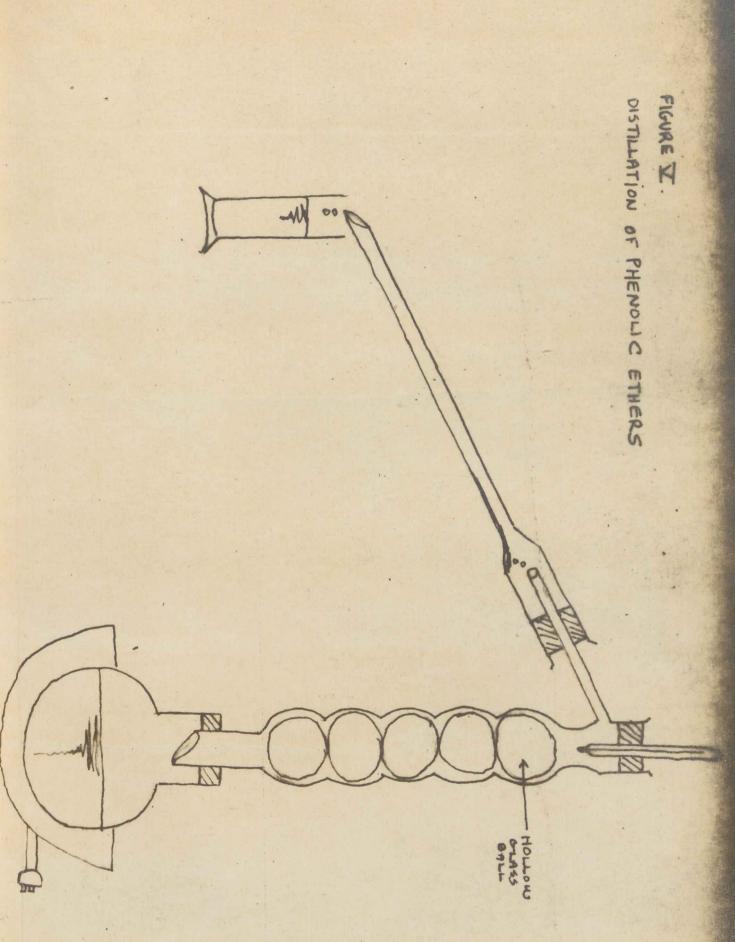
Total volume of gases collected during the run: 21.811ters Volume of gases after adsorption: 13.1 Total volume of butylenes produced during run: 8.7

This volume of butylenes corresponds to 0.388 moles or 11.77 grams of gas produced. A diagram of the adsorption apparatus is shown in figure six.

Identification of Products

Derivitives were made from the cuts obtained during the fractional distillation. Since no literature values for derivitives of sec.-butyl phonols were found, it was found





ELGURE VI BUTYLENE GAS ANALYSIS APPARATUS necessary to prepare derivitives of pure ortho and para secondary butyl phencl, and then compare these with those made of the cuts. Much difficulty was encountered in finding a solid derivitive of these sustituted phenols however, it was found that the p-nitrophenylurethan derivitive gave reproducible results. These derivitives were made according to the method put forth by Shriner and Fuson; however it was found that the addition of two drops of pyridine during the synthesis greatly increased the yield of derivitive. The boiling points of the cuts obtained during fractionation were of some aid in identifying the products.

Thru derivitives and boiling points, ortho and para sec.-butyl phenol sere shown to be formed. From boiling points clone, 2,4-di-sec.-butyl phenol, and ortho and para sec.-butyl phenyl-sec.-butyl other were shown to be present.

Sumary

The reaction between sec.-butyl alcohol and phenol in the vapor phase over an activated alumina catalyst at a temperature of 287°C. was studied.

Fifty per-cent of the phonol was converted; this is in agreement with Perry 13., Lemieux 17., and Putman 18.

The effectiveness of the catalyst remained good for

the whole six hour rum. The larger percentage of products formed consisted of substituted butyl phenols.

Since a large percentage of butyl phenols formed were high boiling and probably polyeubstituted; it is reccommended that for greater yields of monosubstituted butyl phenols a lower temperature should be used for the reaction.



Reaction Run

Activated alumina is used as a catalyst; and a 1:1 molar ratio of sec.-butyl elcohol-phenol feed. A chromel-alumel thermocouple and a Leede and Morthrup potentiometer are used for temperature measurements.

1.	weight	of	feed used	290 Grams
2.	volume	of	food used	515 cc.
5.	weight	of	product at finish	226 grame
4.	volume	of	product at finish	228 cc.
5.	volume	20	gas collected at finish	21.8 liters
6.	weight	or	catalyst used	32.0 grens
7.	volume	of	ontelyst used	36.0 cc.

Data for the reaction run

Tine	Feed Vol. (ml)	Drop Rate per	0" heated feed temp.	*3" (nv.)	**Variac //1 (volts)
10:15	435	33	0.8	9.5	65
10:20	480	27	11.0	11.0	65
10:35	400	10	11.2	11.8	65
10:50	395	85	11.4	11:4	65
11:10	375	20	11.5	11.5	63
11:22	365	25	11.5	11.3	63
11386	360	25	11.1	11.1	63
11:48	355	30	11.5	11.5	65
12:00	355	34	11.1	11.1	63
12:11	325	25	11.5	11.5	65
12:20	315	26	12.0	12,0	57
12:30	305	24	12.0	12:0	53
18:56	300	22	11.6	11.6	53
12:47	295	25	11.5	11.5	50
1:07	880	26	11.0	11.0	52
1:15	275	24	10.8	10.8	58
1:25	263	28	10.5	10.5	52
1:55	255	26	10.5	10.5	54
1:40	245	28	10.5	10.5	54
2:00	835	22	10.5	10.5	55
2:07	230	22	10.5	10.5	55
2:16	225	26	10.3	10.3	55
2:26	210	24	10.2	10.2	55
2:40	201	22	10.0	10.8	55
2:50	195	20	10.8	10:2	57
3:00	190	20	10.0	1010	57
3:20	160	24	10.0	10.0	67
3:27	155	24	10.0	10.0	57
3:45	140	26	10.8	10.2	57
4:00	135	16	10.2	10.2	57
4:15	120	50	20.0	10.0	57

The room temperature was 25°C, and the barometer read 750.0 mm/Ng.

- * This is the temperature at the top of the catalyst bed in millivolts. Additional readings were taken every inch along the reaction tube. Since this is a typical set there is no need to repeat other groups of data.
- Variac #2 corresponded to the readings on variac #1, so again there is no need to present its figures. The rheostat read 3.5 inches throughout the run.

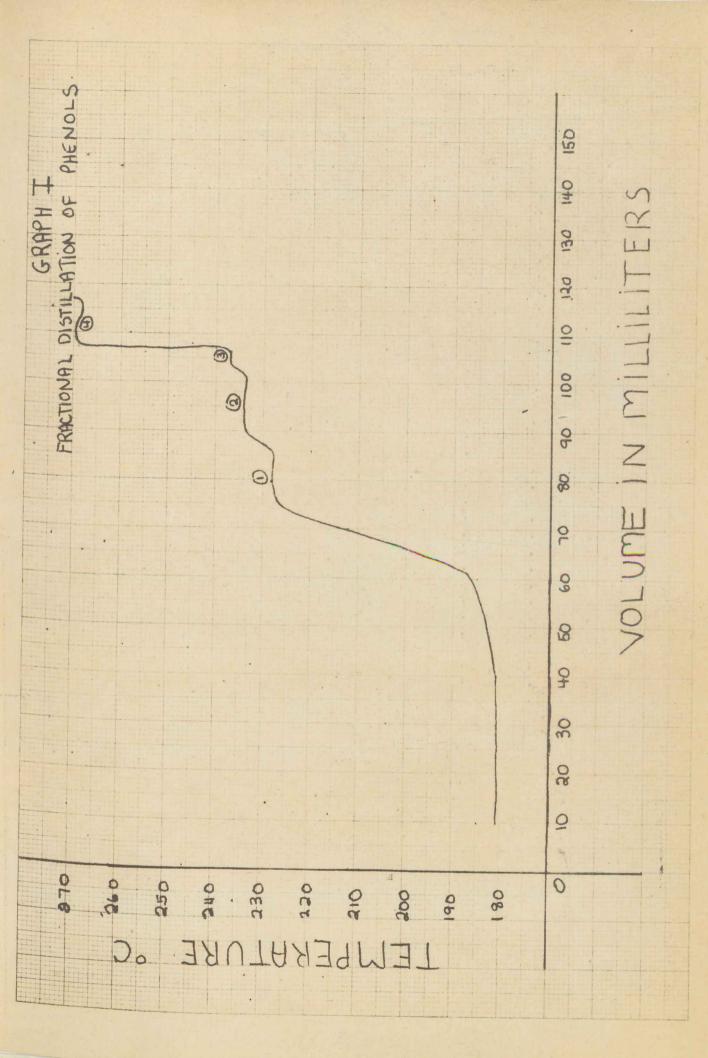
Data for the Fractional Distillation of the Phenols

	Temper		Variaes			1 5 mm 10	(ml.) Total	
Time	Column	Head	Culumn	Pot	Cut#	Vol.	120 001	(Clin)
5:20	175	188	120	80	1	10		W.
3:30	175	188	180	80	î		10.0	
5:40	174	183	100	70		10	20.0	
3:50	180	188	106		1	12	22.0	
4:00	180	182		75	1	7.0	29.0	
4:13	181	103	110	76	1	0.0	55.0	*
79:05	180	183	110	72	1	9.0	44.0	58.5
10:00	177		114	90	2	5.0	47.0	
10:10	181	185	113	70	8	7.0	54.0	10.1
10:16	185	185	150	74	3	1.5	55.5	
10:27		100	118	80	3	2.5	58.0	1.5
10:32	190	192	118	70	4	3.0	61.0	1.0
10:40	198	808	180	78	5	4.0	64.0	1.9
10:45	207	212	120	90	6	1.8	68.0	2,5
10:47	200	210	120	90	17	5.0	69.8	1.1
	213	227	90	90	8	5.0	72.8	8.0
10:50	250	227	90	75	0	8.0	75.8	11 to 10 10 10 10 10 10 10 10 10 10 10 10 10
10:55	230	227	94	75	9	2.5	77.8	
11:00	225	227	100	90	9	8.7	80.3	
11:08	225	231	100	101	9	5.5	85.0	49 - 400
11:15	225	255	100	101	10	5.0		6.5
11:10	289	255	100	101	11	2.5	86.5	2.2
8:05	250	200	200	110	11	2.0	91.5	
10:00	232	255	130	110	18		94.0	6.7
10:18	255	233	110	110	12	8.0	96.0	
10:20	255	256	***	118	12	2.0	98:0	
10:25	238	256	***	118	12	1.5	100.0	
10:42	239	269	130				101.5	3.8
10:45	875	269	130	120	13		104.0	2.7
10:50	276	269		120	14		105.0	4.7
11:05	280	269	130	120	14	1.0	106.5	
11:12	274	269		130	14	1.5	107.5	3
11:20	282	303	130	118	14	2.0	109.0	4.0

25.0 grams of diphenylamine were added as a chaser (B.P. 302°C). At the end of the distillation 24 grams of diphenylamine were left in the stillpot. The barometer read 750mm/Ng.

Weight of product before fractionation: 182 grams
Total weights of cuts 1-14:

Weight loss due to benzene: 76 grams



FRACTIONAL DISTILLATION OF PHENYL ETHERS	3 4 5 6 7 8 9 10 11 12 13 14 15 VOLUME IN MILILITERS
	230 1 230 1 230

Fractionation of Phenolic Ethers

Cut #	. Temp. Oc.	Vol. (ml.)	Total Vol. (ml.)	Wt. (gms.)
	22.0	2.2	2.2	8.0
2	228	2.8	4.4	8.0
1 3	235	8.0	7.4	8.7
4	250	4.0	11.4	5.1
5	250	5.8	15.2	3.0

At start ethers weighed; 86.5 grams Weight of butylphenyl ethers: 13.4 grams Weight less due to water and ethyl ether; 75.1 gms.

Derivitives

I. From pure compounds:

Compound	Melting Point	S Yield -
p-nitrophenylurethan of o-secbutyl phenel	120°0,	92.0
p-nitrophenylurethan of p-sec,-butyl phonol	170	55.0

II. The p-nitrophenylurethan of:

Cut/	Vol.	Boiling range	M.P. of Derivitive	% Yield
9-10	8.7 ml.	22 7- 230°C	137-145	12.5
11-12	6.0	235	137-138	10:0
15	4.0	238 - 259	166-168	5.0
14	7.0	2 75- 288	170	10.0

Physical Constants

Butyl phenol	M.P.	B.P.	n	n 25	Dor.	M.P.	Ref.
0-n		234-7	.975	1,5205	x		1,2,5
n-n		247-9	.974	*	6	67-8	1,5
D-1 1	22	248	. 978	1.4981	a b c	27 21 21 115	1,2,5
0-500.		228 -31 226 - 8	.975	1.5200	bodefa	oil oil oil oil 188 oil	thesis,5,7,8,
y-200.	61-2 53-4	240-8 239-48 236	.966 .986	1.5150 1.5188	a b f	011 011 170 54-5	thesis, 5,7,8,9,11
2,4-d1-	seo.	265-7	.034	1.5072			8
0-tert	96		Control of the Contro				5,6
m-tert	40.6	240		114			5,6
p-tert	09	236 - 8 238 - 5 230	.906	4	b	81-8 86.5	5,8,10,11
0-iso							
m-iso				.0 *			
p-iso		235-9	.980	1.5319	Ъ	124-5	

Entyl phenyl other	B.P.	* 1	125 10	Der.	MePe	Ref.
11	806	.9515	1.5019	h	103-4	2,3,4
sec.	193	.073	1,4943			11
tert.	108		Nr.			11
iso	196	.024	1,4958			11

Code for derivitives:

a	benzoate
b	eryloxyacetic soid
C	phenylurethan
4	a-napthylurothan
0	diphenylurethan
2	p-nitrophenylurethan
S h	p-chlorobenzoa te
h	sulfonamide
1	picrate

All densities are taken at 20°C, with respect to water at 4°C, except where otherwise noted.

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