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## COMMUNICATION

## Highly efficient photocatalytic dehalogenation of organic halides on TiO<sub>2</sub> loaded with bimetallic Pd–Pt alloy nanoparticles<sup>†</sup>

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UV irradiation of TiO<sub>2</sub> loaded with bimetallic Pd–Pt alloy particles promotes highly efficient dehalogenation of organic halides with alcohol as a hydrogen source.

The dehalogenation of organic halides is a significant process for the removal of halogenated organic pollutants and the synthesis of fine chemicals.<sup>1</sup> The reaction is currently carried out *via* the hydrodehalogenation processes with catalysts containing Pd particles using molecular hydrogen (H<sub>2</sub>) as the hydrogen source,<sup>2</sup> which inevitably holds explosion risks. Alternative methods with safe hydrogen sources such as alcohols are therefore desirable.

Recently, a H<sub>2</sub>-free dehalogenation method with alcohol as the hydrogen source was proposed by Fuku *et al.*<sup>3</sup> They employed a photocatalytic reaction using TiO<sub>2</sub> loaded with 1 wt% Pd particles (Pd@TiO<sub>2</sub>). Photoirradiation ( $\lambda > 300$  nm) of a 2-PrOH solution containing chlorobenzene with Pd@TiO<sub>2</sub> and a base (NaOH) produces the corresponding benzene quantitatively. The reactions are initiated by photoexcitation of TiO<sub>2</sub>, producing the electron (e<sup>-</sup>) and positive hole (h<sup>+</sup>) pairs (eqn (1)). The h<sup>+</sup> oxidizes 2-PrOH and produces acetone and protons (eqn (2)).<sup>4</sup> The H<sup>+</sup> is activated by the reduction with e<sup>-</sup> on the Pd particles (eqn (3)), and the formed hydride species (H<sup>-</sup>-Pd) promote dehalogenation (eqn (4)). The removed Cl<sup>-</sup> is solidified as NaCl by the reaction with NaOH (eqn (5)). The overall reaction is expressed as eqn (6).

$$TiO_2 + h\nu \rightarrow h^+ + e^-$$
(1)

$$(CH_3)_2CHOH + 2h^+ \rightarrow (CH_3)_2CO + 2H^+ \qquad (2)$$

$$H^+ + 2e^- + Pd \rightarrow H^- - Pd \qquad (3)$$

$$Ar-Cl + H^{-}-Pd \rightarrow Ar-H + Cl^{-} + Pd \qquad (4)$$

$$H^{+} + Cl^{-} + NaOH \rightarrow H_2O + NaCl \downarrow$$
 (5)

$$Ar - Cl + (CH_3)_2 CHOH + NaOH$$

$$\xrightarrow{h\nu, TiO_2} Ar - H + (CH_3)_2 CO + H_2O + NaCl \downarrow$$
(6)

These reactions proceed at room temperature with alcohol as the hydrogen source, and have a potential to be a safe and sustainable dehalogenation process. The reactions, however, proceed very slowly when compared to the conventional method with  $H_2$ . The activity improvement is therefore necessary.

Herein, we report that  $TiO_2$  loaded with bimetallic Pd–Pt alloy particles (PdPt@TiO<sub>2</sub>) promotes highly efficient photocatalytic dehalogenation. The activity is more than three times that of Pd@TiO<sub>2</sub> and higher than the conventional method with H<sub>2</sub>. The high activity is due to the enhanced consumption of photoformed e<sup>-</sup> on the Pt site by H<sup>+</sup> reduction and efficient transfer of the formed hydrogen atom to the adjacent Pd site within the alloy particles.

 $Pd_1Pt_{\nu}$  (a) TiO<sub>2</sub> with Pd–Pt alloy consisting of 1 wt% Pd  $[=Pd/TiO_2 \times 100]$  and different amounts of Pt [y (wt%) =  $Pt/TiO_2 \times 100$ ] were prepared with Japan Reference Catalyst JRC-TIO-4 TiO<sub>2</sub> (equivalent to Degussa P25) by simultaneous impregnation of Pd(NO<sub>3</sub>)<sub>2</sub> and H<sub>2</sub>PtCl<sub>6</sub> followed by reduction with H<sub>2</sub> (see ESI<sup>†</sup>).<sup>5</sup> A transmission electron microscopy (TEM) image of Pd1Pt5@TiO2 showed spherical metal particles with an average diameter of 2.9 nm (Fig. 1). The lower or higher Pt loadings create smaller or larger particles; Pd<sub>1</sub>Pt<sub>1</sub> and Pd1Pt10 contain 2.5 and 3.4 nm particles, respectively (Fig. S1, ESI<sup>†</sup>). An X-ray photoelectron spectroscopy (XPS) of catalysts confirmed the presence of both Pd and Pt (Fig. S2, ESI<sup>†</sup>). An energy dispersive X-ray spectroscopy (EDX) of metal particles on Pd<sub>1</sub>Pt<sub>5</sub>@TiO<sub>2</sub> (Fig. S3, ESI<sup>†</sup>) determined the average Pt/Pd ratio as 4.95 (wt/wt), which is close to the ratio of the total amount of Pt and Pd (4.96) determined by ICP analysis. An X-ray diffraction (XRD) pattern of Pd1Pt5@TiO2 (Fig. S4, ESI<sup>†</sup>) shows a (111) diffraction of the Pd–Pt alloy at 39.9°, which is located between the Pt(111) and Pd(111) diffractions (39.8° and 40.2°). The lattice parameter of the alloy calculated from the XRD data (a = 0.391 nm) agrees with that calculated with the Vegard's  $law^6$  (0.391 nm). In addition, the d-value calculated from the lattice spacing of the alloy in the TEM image ( $d_{111} = 0.225$  nm, Fig. S5, ESI<sup>†</sup>) is in between the standard Pt ( $d_{111} = 0.2265$  nm, JCPDS 04-0802)

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Fig. 1 (a) TEM image of  $Pd_1Pt_5$ @TiO<sub>2</sub> and (b) size distribution of metal particles on (white) the fresh catalyst and (black) the catalyst recovered after 2nd reuse in reaction (Table 1, run 16).

and Pd ( $d_{111} = 0.2246$  nm, JCPDS 46-1043). These indicate that Pd–Pt alloy particles are indeed loaded on TiO<sub>2</sub>. Diffuse reflectance UV-vis spectra (Fig. S6, ESI†) revealed that Pd<sub>1</sub>Pt<sub>y</sub>@TiO<sub>2</sub> with higher Pt loadings show increased absorbance at >300 nm due to light scattering by the Pt particles.

Table 1 summarizes the results of photocatalytic reaction  $(\lambda > 300 \text{ nm})$  of *p*-chlorotoluene (0.2 mmol) in 2-PrOH (5 mL) with catalysts (5 mg) and NaOH (0.5 mmol) for 1 h at 298 K under Ar. The results obtained using H<sub>2</sub> (1 atm) in the dark at 298 K are also shown for comparison. Both photocatalytic and H<sub>2</sub> systems (runs 1–9) selectively produce toluene. The toluene yields in the photocatalytic system with the catalysts containing Pd alone, Pd<sub>x</sub>@TiO<sub>2</sub> [x (wt%) = Pd/TiO<sub>2</sub> × 100], are less than 21% (runs 1–4). In contrast, the yields in the H<sub>2</sub> system with Pd<sub>x</sub>@TiO<sub>2</sub> are *ca*. 50%, indicating that the photocatalytic system is indeed inefficient.

The loading of Pd–Pt alloy particles significantly enhances the photocatalytic dechlorination (runs 5–9):  $Pd_1Pt_y@TiO_2$ show increased toluene yields with an increase in the Pt amount of the particles, where  $Pd_1Pt_5@TiO_2$  shows the highest yield (76%), which is more than three times that of  $Pd_x@TiO_2$ . In contrast, such alloying effect is not observed in the H<sub>2</sub> system (runs 5–9); the toluene yields decrease monotonically with the Pt loadings (<56%).

It is noted that the catalysts containing Pt alone,  $Pt_y$ @TiO<sub>2</sub> [y (wt%) = Pt/TiO<sub>2</sub> × 100], do not promote dechlorination (runs 10–13). This indicates that, on the alloy catalysts, the Pd site is active for dehalogenation. It is also noted that the Pd–Pt alloy site is necessary for efficient dehalogenation: a Pd<sub>1</sub> + Pt<sub>5</sub>@TiO<sub>2</sub> catalyst (run 14), prepared by a step-by-step deposition of respective Pd and Pt particles (see ESI†), scarcely enhances dehalogenation.

The high activity of the alloy catalyst is due to the efficient consumption of photoformed e<sup>-</sup> by H<sup>+</sup> reduction on the Pt site and efficient transfer of the formed H atom to the adjacent Pd site (Scheme 1a). The efficient e<sup>-</sup> consumption on Pt is confirmed by the amount of formed acetone (Table 1).  $Pd_{x}(a)$  TiO<sub>2</sub> produce <45 µmol acetone (runs 1–4), whereas  $Pt_v @ TiO_2$  produce larger amounts (runs 10–13). This is because e<sup>-</sup> is efficiently trapped by Pt due to the larger work function<sup>7</sup> and consumed by  $H^+$  reduction, facilitating efficient alcohol oxidation by h<sup>+</sup>. As shown in run 12, Pt<sub>5</sub>@TiO<sub>2</sub> produces the largest amount of acetone among Pt<sub>v</sub>@TiO<sub>2</sub> and higher Pt loadings decrease the production. A similar tendency is observed for Pd<sub>1</sub>Pt<sub>v</sub>@TiO<sub>2</sub>: Pd<sub>1</sub>Pt<sub>5</sub> produces the largest amount of acetone. The higher activity of  $Pd_1Pt_5$  (a) TiO<sub>2</sub> than Pd (a) TiO<sub>2</sub> is thus because the photoformed  $e^-$  is efficiently consumed by  $H^+$  reduction on the Pt site, producing a H atom.<sup>8</sup>

$$H^{+} + e^{-} + Pt \rightarrow H - Pt \qquad (7)$$

The H atom on Pt within the alloy particles is efficiently used for dehalogenation. This is confirmed by the  $H^+$  balance, defined as the ratio of the formed dehalogenation product to that of the formed  $H^+$ . As shown by eqn (6), two  $H^+$  formed

 Table 1
 Results of dechlorination of p-chlorotoluene in the photocatalytic and H<sub>2</sub> systems<sup>a</sup>

	( <i>photocatalytic system</i> ) catalyst (5 mg), 2-PrOH (5 ml), NaOH (0.5 mmol) Ar (1 atm), λ >300 nm, 298 K, 1 h	► I
0.2 mmol	(H <sub>2</sub> system) catalyst (5 mg), 2-PrOH (5 ml), NaOH (0.5 mmol) H <sub>2</sub> (1 atm), dark, 298 K, 1 h	

Run	Catalyst	Metal particle size <sup>b</sup> /nm	Photocatalytic system				H <sub>2</sub> system	
			<i>p</i> -Chlorotoluene conv. (%)	Toluene yield (%)	Acetone formed/µmol	$H^+$ balance <sup>c</sup>	<i>p</i> -Chlorotoluene conv. (%)	Toluene yield (%)
1	Pd <sub>1</sub> @TiO <sub>2</sub>	5.3	20	19	42	0.92	56	54
2	Pd <sub>3</sub> @TiO <sub>2</sub>		21	20	43	0.96	56	54
3	Pd <sub>5</sub> @TiO <sub>2</sub>		19	18	41	0.88	52	51
4	Pd <sub>7</sub> @TiO <sub>2</sub>		14	13	29	0.90	35	34
5	$Pd_1Pt_1@TiO_2$	2.5	28	27	55	0.97	32	31
6	$Pd_1Pt_3 @ TiO_2$		45	43	88	0.97	26	23
7	$Pd_1Pt_5 @ TiO_2$	2.9	76	76	155	0.98	21	20
8	$Pd_1Pt_7@TiO_2$		39	38	80	0.95	15	13
9	$Pd_1Pt_{10} @ TiO_2$	3.4	36	35	79	0.90	12	11
10	$Pt_1 @ TiO_2$	2.2	0	0	43		0	0
11	$Pt_3 @ TiO_2$		0	0	65		0	0
12	Pt <sub>5</sub> @TiO <sub>2</sub>	3.9	0	0	102		0	0
13	$Pt_7@TiO_2$		0	0	79		0	0
14	$Pd_1 + Pt_5@TiO_2$		27	26	118	0.44	26	25
$15^d$	Pd <sub>1</sub> Pt <sub>5</sub> @TiO <sub>2</sub>		75	75	-		-	-
$16^e$	$Pd_1Pt_5@TiO_2$	3.1 <sup>f</sup>	75	75				

<sup>*a*</sup> The results obtained with Pd<sub>1</sub>Pt<sub>5</sub>@TiO<sub>2</sub> in other solvents are summarized in Table S1 (ESI†). <sup>*b*</sup> TEM micrographs and the size distributions are shown in Fig. S1 (ESI†). <sup>*c*</sup> Determined by eqn (8). <sup>*d*</sup> 1st reuse after washing with 2-PrOH. <sup>*e*</sup> 2nd reuse. <sup>*f*</sup> Measured after 2nd reuse.

99

57

99

76

97

75

96

> 99

>99

>99

58

77

76

97



Scheme 1 The reaction sequence for protons on the metal particles of (a)  $Pd_1Pt_5@TiO_2$  and (b)  $Pd_1 + Pt_5@TiO_2$  catalysts.

by photooxidation of 2-PrOH are consumed by dehalogenation (eqn (3) and (4)) and reaction with NaOH (eqn (5)), respectively. The H<sup>+</sup> balance is therefore expressed by the ratio of the amount of formed toluene to that of formed acetone,

$$H^+$$
 balance = [toluene formed]/[acetone formed] (8)

Table 1 summarizes the H<sup>+</sup> balance for the respective systems obtained by photoreaction for 1 h. The values for Pd<sub>x</sub>@TiO<sub>2</sub> are almost 1 (runs 1–4), indicating that H<sup>+</sup> formed by alcohol oxidation are consumed quantitatively by dehalogenation on Pd (eqn (6)).<sup>3</sup> The values for PdPt@TiO<sub>2</sub> are also almost 1 (runs 5–9), suggesting that  $H^+$  are also consumed quantitatively although  $H^+$  are reduced on Pt (eqn (7)). The results suggest that, as shown in Scheme 1a, the H atom formed on Pt is transferred to the adjacent Pd site (H-Pd formation), which is probably due to the stronger H-Pd interaction.9

$$H-Pt \rightarrow H-Pd$$
 (9)

The H atom is reduced to the hydride species  $(H^--Pd)$  by  $e^-$ , which promotes dechlorination (eqn (4)).

$$H-Pd + e^{-} \rightarrow H^{-}-Pd \tag{10}$$

As shown in run 14, the  $H^+$  balance for the  $Pd_1 + Pt_5@TiO_2$ system is only 0.44. This is because the absence of Pd around the Pt site suppresses the H transfer from Pt to Pd and results in removal of H atoms by H<sub>2</sub> formation (Scheme 1b).<sup>10</sup>

$$H-Pt + H-Pt \rightarrow H_2\uparrow + 2Pt$$
(11)

Change in H<sub>2</sub> amount during reaction confirms this (Fig. S7, ESI<sup> $\dagger$ </sup>). Pd<sub>1</sub> + Pt<sub>5</sub>@TiO<sub>2</sub> promotes H<sub>2</sub> formation and dechlorination simultaneously; however,  $Pd_1Pt_5@TiO_2$ scarcely produces H<sub>2</sub> until *p*-chlorotoluene disappears. The alloy sites are therefore necessary for efficient H transfer from the Pt to Pd sites.

The above results reveal that, on the alloy site (Scheme 1a), efficient reduction of H<sup>+</sup> by e<sup>-</sup> on Pt, smooth H transfer to Pd, and reduction of H by e<sup>-</sup> occur sequentially. This sequence produces a large amount of H<sup>-</sup>-Pd species and promotes efficient dehalogenation. It must be noted that, as shown in runs 15 and 16 (Table 1), the alloy catalyst is reusable for dehalogenation at least two times without loss of activity and selectivity. In addition, as shown in Fig. 1b, the size of Pd-Pt alloy particles scarcely changes even after the reaction.

The alloy catalyst is tolerant for photocatalytic dehalogenation of various aromatic halides (Table 2). Pd1Pt5@TiO2 produces the corresponding dehalogenation compounds with very high yield, and the catalytic activities are much higher than those obtained with  $Pd_1$  (*i*)  $TiO_2$  using  $H_2$ .

 Table 2
 Dehalogenation of various aromatic halides

Photo

Photo

Photo

Photo

 $H_2$ 

H<sub>2</sub>

 $H_2$ 

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3

4

5

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8

9

10

11

progress.

p	(photocata	ohotocatalytic system) Pd₁Pt₅@TiO₂ (5 mg) 2-PrOH (5 ml), NaOH (0.5 mmol) Ar (1 atm), λ >300 nm, 298 K				
R <sub>1</sub> U (H <sub>2</sub> system) Pd <sub>1</sub> Pt <sub>0</sub> @TiO <sub>2</sub> (5 mg) 0.1 mmol 2-PrOH (5 ml), NaOH (0.5 mmol) H <sub>2</sub> (1 atm), dark, 298 K						
Run	Substrate	System	Time/h	Conv. (%)	Yield (%)	
		Photo	1.5	99	97	
2	$\lor$	$H_2$	1.5	74	72	
;	CI	Photo	1	>99	99	
Ļ	$\mathbf{V}$	$H_2$	1	52	51	

1

1

1

1

2

12	$\bigcirc$	$H_2$	2	51	49
13		Photo	2	92	87 (toluene)
14		$H_2$	2	60	37 (toluene)
In	ı summary, w	ve found t	hat UV	irradiation o	f TiO <sub>2</sub> loaded
with	Pd–Pt allo	y promo	tes effici	ent dehalog	enation. This
offer	rs crucial adv	vantages:	(i) safe a	alcohols can	be used as a
hydı	rogen source;	and, (ii)	the react	tion proceeds	s much faster.
The	alloy catal	yst that	facilitate	s efficient p	production of
activ	ve species (H <sup>-</sup>	–Pd) may	also pro	omote other h	nydrogenation
reac	tions, and t	he work	along th	hese lines is	currently in

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