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1 Ultrasound increases the aqueous extraction of phenolic compounds with
2 high antioxidant activity from olive pomace.

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14

15 **Abstract**

16 Olive pomace is a waste produced by the olive oil industry in massive quantities each year. Disposal
17 of olive pomace is difficult due to high concentrations of phenolic compounds, which is an
18 environmental concern. However, phenolic compounds have applications in the health industry.
19 Therefore, extraction of phenolic compounds from olive pomace has the potential to remove an
20 environmentally hazardous portion of pomace while creating an additional source of income for
21 farmers and producers. Using advanced technologies including Ultrasound Assisted Extraction
22 (UAE), combined with water as an extraction solvent, has recently gained popularity. The present
23 study outlines the optimal UAE conditions for the extraction of phenolic compounds with high
24 antioxidant activity from olive pomace. Optimal conditions were developed using RSM for
25 parameters power, time and sample-to-solvent ratio. Total phenolic compounds determined by Folin
26 Ciocalteu method and total major bioactive compounds determined by HPLC as well as antioxidant
27 capacity (DPPH and CUPRAC) were investigated. The optimal conditions for the extraction of
28 phenolic compounds with high antioxidant activity were 2 g of dried pomace/ 100mL of water at
29 250W power for 75mins. UAE improved the extraction efficiency of water and yielded extracts with
30 high levels of phenolic compounds and strong antioxidant activity.

31

32 **Keywords**

33 Olive pomace; *Olea Europaea*; HPLC; UAE; Response Surface Methodology.

34

35 **1. Introduction**

36 Olive pomace is the solid waste product of the olive oil extraction process, which retains high
37 amounts of organic substances (14-15%), including sugars, nitrogenous compounds, volatile
38 fatty acids, polyalcohols, pectins and fats (Lafka, Lazou, Sinanoglou, & Lazos, 2011) as well

39 as a high concentration of phenolic compounds (Goldsmith, Vuong, Stathopoulos, Roach, &
40 Scarlett, 2014a; Ranalli, Lucera, & Contento, 2003). Thousands of tonnes of olive waste are
41 produced each year; these waste products are often dumped in landfill, which is causing a
42 number of environmental concerns due to the presence of phenolic compounds. Therefore,
43 the disposal of olive waste products has been a major environmental issue in a number of
44 olive growing countries (Capasso, Cristinzio, Evidente, & Scognamiglio, 1992).

45 Extraction of the phenolic compounds from olive pomace has the potential to somewhat limit
46 the environmental damage that can be caused by this waste fraction and may even provide an
47 additional source of income for olive oil producers (Obied, Allen, Bedgood, Prenzler, &
48 Robards, 2005). For example, the extraction of oleuropein, the most abundant phenolic
49 compound in olive products, would add value to the olive oil production process. This is
50 because a number of the beneficial health effects of virgin olive oil have been attributed to
51 consumption of oleuropein, including anti-atherogenic (Covas, 2007), anti-inflammatory (de
52 la Puerta, Ruiz Gutierrez, & Hault, 1999), anti-cancer (Ahmad Farooqi et al., 2017; Fayyaz et
53 al., 2016; Hadrich et al., 2016; Liu, Wang, Huang, Chen, & Li, 2016; Maalej, Bouallagui,
54 Hadrich, Isoda, & Sayadi, 2017; Morana et al., 2016; Secme, Eroglu, Dodurga, & Bagci,
55 2016; Sepporta et al., 2016; Xu & Xiao, 2017) and anti-microbial (Bisignano et al., 1999)
56 properties and therefore oleuropein is a valuable product in itself. A number of advanced
57 techniques to extract phenolic compounds have gained popularity in recent years including
58 Microwave Assisted Extraction (MAE), Pressurised Liquid Extraction (PLE) and Solid Phase
59 Extraction (SPE). However, Ultrasound Assisted Extraction (UAE) is considered one of the
60 simplest and most cost-effective techniques to scale up for industrial production.

61 The UAE method has been used to improve the extraction efficiency of phenolic compounds
62 from a variety of plant matrices. The method has a number of benefits, including as an add on
63 step to existing processes with minimum alteration, as an application in the aqueous

64 extraction of phenolic compounds therefore reducing the need for harmful organic solvents,
65 which can be difficult and expensive to dispose of. The UAE method often results in shorter
66 extraction times and high yields; importantly, UAE has been shown to improve extraction
67 yield up to 35% (Vilkhu, Mawson, Simons, & Bates, 2008).

68 Despite the clear benefits of UAE, the use of high power levels with the method can lead to
69 the degradation of phenolic compounds. For example, in one of our previous studies we
70 observed a 25% decrease in the extraction of Euphol from Euphorbia Tirucalli when the
71 power was increased from 150-250W (2015). Therefore, it is important to optimise the UAE
72 extraction parameters to ensure the maximum retention of valuable compounds.

73 Water is classified as a safe and “green” solvent, which is inexpensive, accessible and
74 considered an environmentally friendly alternative to harmful organic solvents (Hartonen &
75 Riekkola, 2017). Therefore, water was the solvent of choice for the recovery of bioactive
76 compounds from olive pomace in the present study. This study, for the first time, optimised
77 the Ultrasound Assisted Extraction (UAE) conditions for maximum recovery of phenolic
78 compounds with high antioxidant activity from olive pomace using water. Our study is the
79 first to investigate water as an extraction solvent and determine the optimal conditions for the
80 extraction of bioactive compounds from olive pomace.

81

82

83 **2. Materials and Methods**

84 *2.1. Materials and Reagents*

85 Folin–Ciocalteu’s reagent, sodium carbonate, gallic acid, 1,1-diphenyl-2-picrylhydrazyl
86 (DPPH), 6-hydroxy-2,5,7,8-tetramethylchroman-2-carboxylic acid (trolox), 2,4,6-Tris(2-

87 pyridyl)-s-triazine (TPTZ), ferric chloride, sodium acetate, acetic acid, copper (II) chloride,
88 ammonium acetate (NH₄Ac), neocuproine methanol and ethanol were purchased from Sigma
89 Aldrich (Castle Hill, NSW, Australia). Ultra-pure (type 1) de-ionized (DI) water was prepared
90 by reverse osmosis and filtration using a Milli-Q direct 16 system (Millipore Australia Pty
91 Ltd., North Ryde, NSW, Australia).

92 *2.2. Sample Collection and preparation*

93 Green olives of the Manzanilla cultivar were harvested at Houndsfield Estate (Hunter Valley,
94 NSW, Australia) in July 2015 and processed on-site the next day using a semi-continuous
95 Enorossi 150 traditional olive oil pressing system (Enoagricola Rossi, Calzolaro di
96 Umbertide, Perugia, Italy) standardised to press a maximum of 150kg of olives at a time.
97 Olive pomace was collected and stored at -20°C until further analysis. Olive pomace was
98 freeze dried until constant weight was achieved before blending in a blender and being passed
99 through a 0.1mm sieve and stored at -20°C until further analysis. Dried pomace was then de-
100 fatted 3 times by adding 100mL of hexane to 10g of pomace and filtering with a Buchner
101 funnel apparatus. For extraction yields, the water was removed from a certain quantity of
102 extract in a vacuum drier (Mettler, Schwabach, Germany) at 50 °C and vacuum pressure
103 of 65 mb until constant weight was achieved (total aqueous extract yield = 208.35 ± 35 mg/g
104 dried sample).

105 *2.3. Response Surface Methodology (RSM)*

106 The RSM with the Box–Behnken design was used to investigate the influence of three
107 independent parameters; power, time and sample to solvent ratio, on the extraction of total
108 phenolic compounds (TPC) and the antioxidant activity of the extracts. An ultrasonic bath
109 was used (Soniclean, 220V, 50Hz and 250W model 250HD, Soniclean, Pty Ltd, Thebarton,
110 SA, Australia). The optimal ranges of power (150-250W), time (45-75 min) and sample-to-

111 solvent ratio (1-3 g/100 mL) were determined based on preliminary experiments (data not
112 shown). A control extraction was conducted at the same optimal time and sample to solvent
113 ratio without ultrasound. Temperature was maintained at 40°C by the ultrasound baths
114 temperature regulator. The independent variables and their code variable levels are shown in
115 Table 1.

116 To express the TPC or antioxidant capacity as a function of the independent variables, a
117 second-order polynomial equation was used as follows and as previously described by Vuong
118 *et al.* (2011):

$$119 \quad Y = \beta_0 + \sum_{i=1}^k \beta_i X_i + \sum_{i=1}^{k-1} \sum_{j=i+1}^k \beta_{ij} X_i X_j + \sum_{i=1}^k \beta_{ii} X_i^2,$$

120 Where various X_i values are independent variables affecting the response Y ; β_0 , β_i , β_{ii} , and β_{ij}
121 are the regression coefficients for the intercept and the linear, quadratic and interaction terms,
122 respectively, and k is the number of variables.

123 *2.4. Total Phenolic Compounds*

124 The TPC were determined according to Thaipong *et al.* (Thaipong, Boonprakob, Crosby,
125 Cisneros-Zevallos, & Hawkins Byrne, 2006). Briefly, samples were added to Folin–
126 Ciocalteu’s reagent before adding 5% sodium carbonate solution and incubating in the dark
127 for 1h. Absorbance was then read at 760nm using a UV spectrophotometer (Varian, Melbourne,
128 VIC, Australia). Results were expressed as mg of gallic acid equivalents per gram of dried
129 olive pomace (mg GAE/g).

130 *2.5. Total Major Bioactive Compounds*

131 For determination of total major bioactive compounds, HPLC was performed according to
132 Goldsmith *et al.*, (2014a) with minor modifications. The extracts were analysed using a

133 Shimadzu HPLC system (Shimadzu Australia, Rydalmere, NSW Australia) and a 250 ±
134 4.6mm Synergi 4 µm Fusion-RP 80A reversed-phase column (Phenomenex Australia Pty.
135 Ltd., Lane Cove, NSW Australia) with detection at 254nm. The column was maintained at
136 30°C, the flow rate was 1 ml/min and three solvents were used for the mobile phase Solvent
137 **A**: 0.1% orthophosphoric acid, Solvent **B**: 100% Methanol, Solvent **C**; 100% Ethanol. A
138 gradient elution schedule was used according to the following: 0-40 mins A 96%, B 2%, C
139 2%; 40-60 mins A 40%, B 30%, C 30%; 60-62 mins A 96%, B 2%, C 2%. Syringic acid was
140 used as internal standard. Values for total major bioactive compounds were determined using
141 a tyrosol standard curve; they were expressed as µg Tyrosol equivalents (TYE) per gram of
142 dried olive pomace.

143

144 *2.6. Antioxidant Activity Assays*

145 Two assays were employed to assess the antioxidant activity of the pomace extracts:
146 The cupric reducing antioxidant capacity (CUPRAC) assay was conducted as previously
147 described by Apak *et al.* (2004). Results were expressed as mg of trolox equivalents per gram
148 of dried olive pomace (mg TRE/g).

149 The DPPH free radical scavenging capacity of the extracts were analysed using the
150 1,1-diphenyl-2-picrylhydrazyl (DPPH) assay, as described by Goldsmith *et al.* (2014b). The
151 results were expressed as mg of trolox equivalents per gram of dried olive pomace (mg
152 TRE/g).

153

154 *2.7. Statistical analysis*

155 The RSM was designed and analysed using JMP Version 11 (SAS Cary, NC, USA). JMP
156 was also used to develop the model equation, graph the 2D and 3D prediction profiler plots to
157 predict the optimum values of the response variables in order to maximise the TPC and

158 antioxidant capacity of the extracts. The original values and ranges of the parameters under
159 investigation as well as their parameter symbols and codes are presented in *Table 1*.

160

161 **3. Results and discussion**

162 *3.1. Fitting the models for the prediction of TPC and antioxidant capacity*

163 Based on preliminary experiments (not shown), time, power and sample-to-solvent ratio were
164 identified as important parameters which could impact upon the extraction of phenolic
165 compounds from olive pomace, the ranges for each variable were determined and are listed in
166 *Table 1*.

167 *Table 2* shows the reliability of the mathematical model in predicting variances between
168 actual and predicted values. The analysis of variance for the experimental results for the Box
169 Behenkin design showed the coefficient of determination (R^2) for the fit of the model of TPC
170 was 0.8, CUPRAC was 0.81 and DPPH was 0.69; suggesting that 80%, 81% and 69% of the
171 actual TPC, CUPRAC and DPPH values could be predicted by the model, respectively. This
172 relationship is further supported by the values for Predicted Residual Sum of Squares
173 (PRESS is a measure of how well each point fits the experimental design) and the F-ratio of
174 the model: 3128 and 15.1 for TPC, 3001 and 6.56 for CUPRAC and 1566 and 6.15 for DPPH
175 (respectively). In summary, analysis of variance showed that the models are reliable for
176 prediction of TPC and antioxidant capacity.

177 *3.2. The effect of the test parameters on the extraction of TPC*

178 The effect of the test parameters (coded variables in *Table 1*) on the response variable (Y)
179 TPC is shown in the following equation:

180 $Y = 8.3 + 2.4 X_1 + 0.1 X_2 - 0.7 X_3 + 1.6 X_1 X_2 - 1.0 X_1 X_3 - 1.1 X_2 X_3 + (6.2 X_1)^2 + (3.5 X_2)^2 - (2.6$
181 $X_3)^2$

182 **Table 3** presents the linear regression coefficients for each variable and indicates their
183 statistical significance. Power and time both had positive relationships with the extraction of
184 TPC, while the sample-to-solvent ratio had a negative effect; that is, as we increased the
185 amount of sample while keeping the amount of solvent that same, we saw a decrease in TPC.
186 Therefore, as power and time were increased and as the amount of solvent /g of sample were
187 increased, the extraction of TPC also increased. However, the only individual variable that
188 had a significant influence on the extraction of TPC within the ranges tested was power (p =
189 0.0001). Power has previously been shown to increase the extraction of phenolic compounds
190 from a variety of sources (Altemimi, Watson, Choudhary, Dasari, & Lightfoot, 2016).
191 Moreover, the combination of power and time also had a significant influence on the
192 extraction of TPC (p = 0.03); this is also in accordance with the literature (Falleh, Ksouri,
193 Lucchessi, Abdelly, & Magné, 2012). In addition, the interaction between power and time
194 within the ranges tested had a significant impact on extraction of TPC whereas, there was no
195 interactive relationship between power and ratio or time and ratio (Table 3); indicating that
196 increasing both power and time can result in a higher TPC being extracted from the olive
197 pomace.

198

199 *3.3. The effect of the test parameters on antioxidant activity*

200 The effect of the test parameters (coded variables in Table 1) on the response variable DPPH
201 scavenging capacity (Y) is shown in the following equation:

202 $Y = 22.4 + 2.5 X_1 + 0.3 X_2 + 5.7 X_3 + 3.6 X_1 X_2 - 0.9 X_1 X_3 - 3.0 X_2 X_3 + (1.3 X_1)^2 - (3.8 X_2)^2 -$
203 $(0.2 X_3)^2$

204 Similarly, the effect of the test parameters (coded variables in Table 1) on the response
205 variable cupric reducing antioxidant capacity (Y), is shown in the following equation:

206 $Y = 37 + 6.8 X_1 + 1.6 X_2 - 0.9 X_3 + 4.8 X_1 X_2 - 1.6 X_1 X_3 - 6.3 X_2 X_3 + (19.9 X_1)^2 + (10.4 X_2)^2 -$
207 $(5.1 X_3)^2$

208 The results showed that the individual variables of power and time had a positive influence
209 on both the DPPH scavenging capacity and the cupric reducing antioxidant capacity of the
210 extracts. Sample-to solvent ratio on the other hand, had a positive influence on the DPPH
211 scavenging capacity but had a negative influence on the cupric reducing antioxidant capacity.
212 In addition, power and time as well as time and sample to solvent ratio, in the tested ranges,
213 had a significant interactive effect on DPPH scavenging capacity and the cupric reducing
214 antioxidant capacity of the extracts. Of interest, power and ratio in the tested ranges did not
215 show a significant interactive effect on DPPH scavenging capacity and cupric reducing
216 antioxidant capacity of the extracts.

217 *3.4. Optimisation of the extraction conditions for maximum extraction of TPC with high*
218 *antioxidant activity from olive pomace*

219 Based on the predictive models (Figures 1 and 2), the optimal conditions for the extraction of
220 phenolic compounds from olive pomace were 2g of dried pomace/ 100mL of water at 250W
221 power for 75mins. These conditions were the same for the optimisation of antioxidant activity
222 via DPPH and CUPRAC; therefore, these conditions were used for further validation (Table
223 4). The resulting values fell inside the proposed ranges for TPC and antioxidant activity. As

224 such, these conditions were proposed as optimal for the extraction of phenolic compounds
225 with high antioxidant activity from olive pomace waste.

226 *3.5. Optimal UAE conditions compared to control conditions*

227 The principle of UAE extraction is to disrupt plant cell walls and increase mass transfer of
228 intracellular components into the extraction solvent (Yingngam, Monschein, & Brantner,
229 2014). To assess the efficacy of ultrasound in extracting phenolic compounds with high
230 antioxidant activity from olive pomace, validation was also conducted comparing the optimal
231 conditions with and without ultrasound. The optimised UAE conditions increased the
232 extraction of TPC by 24% (Table 4). This was also reflected in the HPLC results where by
233 the UAE improved total peak area by 20.4% (Table 5). Typical chromatograms produced
234 from optimised UAE extracts as well as control extracts are pictured in Figure 3. The UAE
235 conditions yielded a higher level of TPC as well as antioxidant activity compared to the
236 control. Figure 3 shows that the optimised UAE extracts had a higher area for most of the
237 peaks compared to the control extracts; however, the UAE extracts did not have any
238 additional peaks. This suggests that UAE enhanced the ability of water to extract compounds
239 from the pomace without extracting any additional compounds. This increase can be
240 attributed to the ability of Ultrasound to impact the microstructure of plant materials; since
241 ultrasonic cavitation creates shear forces that disrupt cell walls, which enabled the extraction
242 solvent to penetrate the pomace tissue and extract the phenolic compounds. Similar results
243 have been reported previously (Chen et al., 2018; Feng, Luo, Tao, & Chen, 2015; Tian, Xu,
244 Zheng, & Martin Lo, 2013).

245

246 The antioxidant activity of the UAE extracts (Table 4) was also higher than the controls (an
247 increase of 11% and 12% for the DPPH and CUPRAC assays respectively). The application
248 of UAE has been shown to increase the antioxidant activity of extracts from a variety of plant

249 materials, including olive leaves (Sahin & Samli, 2013), peach, pumpkin (Altemimi et al.,
250 2016) and green tea (Nkhili et al., 2009). This is likely due to the improvement in the
251 extraction of total phenolic compounds. In the present study, no new peaks were identified in
252 the chromatograms from the UAE extracts (Figure 3) when compared to the controls;
253 therefore, the increase in antioxidant activity is likely due a larger quantity of each compound
254 being extracted. However, since the peak area (mg TYE equivalents) increased by 26% with
255 the application of UAE (Table 4) the peaks that were significantly increased must correspond
256 to compounds with high antioxidant activity. Therefore, UAE can be considered as an
257 effective technique to increase the levels of the extracted compounds with high antioxidant
258 activity in olive pomace extracts.

259

260 **4. Conclusions**

261 UAE increased the quantity of phenolic compounds extracted from olive pomace. The
262 proposed optimal conditions for the extraction of phenolic compounds with high antioxidant
263 activity from olive pomace were 2 g of dried pomace/ 100mL of water at 100% power
264 (250W) for 75mins maintained at 30°C. This simple and inexpensive method could be readily
265 up-scaled to add a source of income to olive farmers and olive oil processors, a viable use for
266 this agricultural waste product.

267

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- 1 **Table 1.** Values of the independent parameters and their coded forms with their symbols employed in
 2 RSM for optimization of UAE conditions for phenolic compounds from olive pomace.

Independent Parameters	Symbols of the Parameters	Original Values of the Parameters	Parameter Coded Forms*
Power (W)	X_1	100	-
		150	0
		250	+
Time (min)	X_2	45	-
		60	0
		75	+
Ratio (g/100mL)	X_3	1	-
		2	0
		3	+

- 3 *Parameter coded forms -, 0 and + are the minimum point, centre point and maximum point
 4 (respectively) for the independent parameters temperature, time and ratio.

5

Table 2. Analysis of variance for determination of the model fit. Total Phenolic Compounds (TPC) and antioxidant capacity (CUPRAC and DPPH).

Sources of Variation	TPC	Antioxidant Capacity	
		CUPRAC	DPPH
Lack of fit (<i>p</i> -value)	>0.0001*	>0.0001*	0.0076*
R^2	0.8	0.81	0.69
PRESS	3128	3001	1566
F-ratio of model	15.1	6.56	6.15
<i>p</i> of model > F	>0.0001*	>0.0001*	>0.0001*

* Denotes significant result ($p < 0.05$)

Table 3. The analysis of variance for the experimental results.

Parameter	DF	TPC		Antioxidant Capacity			
				DPPH		CUPRAC	
		Estimate	Prob> F	Estimate	Prob> F	Estimate	Prob> F
β_0	1	8.26	<0.0001*	22.4	<0.0001*	37.14	<0.0001*
$\beta_{1\text{ power}}$	1	2.4	<0.0001*	2.53	0.0288*	6.79	<0.0001*
$\beta_{2\text{ time}}$	1	0.068	0.89	0.29	0.7921	1.61	0.2950
$\beta_{3\text{ ratio}}$	1	-0.70	0.11	5.68	<0.09	-0.91	0.4832
$\beta_{12\text{ power.time}}$	1	1.59	0.025*	3.64	0.0209*	4.81	0.0250*
$\beta_{13\text{ power.ratio}}$	1	-0.97	0.10	-0.92	0.4758	-1.60	0.3650
$\beta_{23\text{ time.ratio}}$	1	-1.12	0.065	-2.96	0.0272*	-6.33	0.0009*
$\beta_{11\text{ power}^2}$	1	6.24	<0.0001*	1.26	0.4260	19.93	<.0001*
$\beta_{22\text{ time}^2}$	1	3.53	<0.0001*	-3.79	0.0210*	10.37	<.0001*
$\beta_{33\text{ ratio}^2}$	1	-2.62	0.0026*	-0.24	0.8914	-5.06	0.0445*

* Significantly different at $p < 0.05$; β_0 : intercept; β_1 , β_2 and β_3 : linear regression coefficients for power, time and ratio; β_{12} , β_{13} and β_{23} : regression coefficients for interaction between power \times time, power \times ratio and time \times ratio; β_{11} , β_{22} and β_{33} : quadratic regression coefficients for power \times power, time \times time and ratio \times ratio.

Table 4. Validation of the RSM models; the predicted values and the actual values obtained at the maximum desirability for the UAE conditions of 2 g of dried pomace/ 100mL of water at 100% power for 75 min maintained at 30°C.

	Phenolic compounds	Antioxidant activity	
	TPC	DPPH	CUPRAC
	(mg GAE g ⁻¹)	(mg TRE g ⁻¹)	(mg TRE g ⁻¹)
Predicted	22.02 ± 2.66 ^a	26.37 ± 5.85 ^a	80.57 ± 7.99 ^a
Actual (UAE)	19.71 ± 1.41 ^a	31.23 ± 1.42 ^a	73.54 ± 2.54 ^a
Control (no UAE)	13.76 ± 0.91 ^b	28.07 ± 3.24 ^a	65.36 ± 1.77 ^b

^{a, b} Values in the same column with a different superscript are significantly different from one another (p<0.05)

Total yield of extracts (UAE = 222.2 ± 48.1, Control = 194 ± 39.6)

Table 5. Quantification of selected HPLC peaks expressed as μM Tyrosol Equivalents (TYE)/g of dried pomace. Peak numbers correspond to the peaks in Figure 3.

<i>Peak number</i>	<i>Retention time</i> (mins)	<i>UAE</i> (μM TYE/g)	<i>Control</i> (μM TYE/g)
1	7.20	0.95 ± 0.1^a	0.46 ± 0.07^b
2	8.46	13.65 ± 0.84^a	10.01 ± 0.12^b
3	10.14	1.38 ± 0.02^a	0.64 ± 0.06^b
4	12.27	0.08 ± 0.03^a	0.00^b
5	16.26	6.24 ± 1.01^a	4.99 ± 0.03^b
6	16.89	1.29 ± 0.01^a	0.61 ± 0.04^b
7	17.41	0.00^a	0.69 ± 0.07^b
8	19.47	20.01 ± 0.04^a	15.87 ± 0.09^b
9	19.98	5.68 ± 0.07^a	4.22 ± 0.03^b
10	22.74	2.24 ± 0.12^a	1.58 ± 0.15^b
11	23.86	3.95 ± 0.01^a	2.86 ± 0.49^b
12	24.69	0.80 ± 0.01^a	0.76 ± 0.31^a
IS	26.11	na	na
13	31.46	3.76 ± 0.25^a	0.72 ± 0.24^b
14	42.91	5.78 ± 0.05^a	5.21 ± 0.73^a
Total		62.05 ± 1.87^a	49.98 ± 2.27^b

^{a, b} Values are means \pm SD in the same row with a different superscript are significantly different from one another ($p < 0.05$).

Figure 1

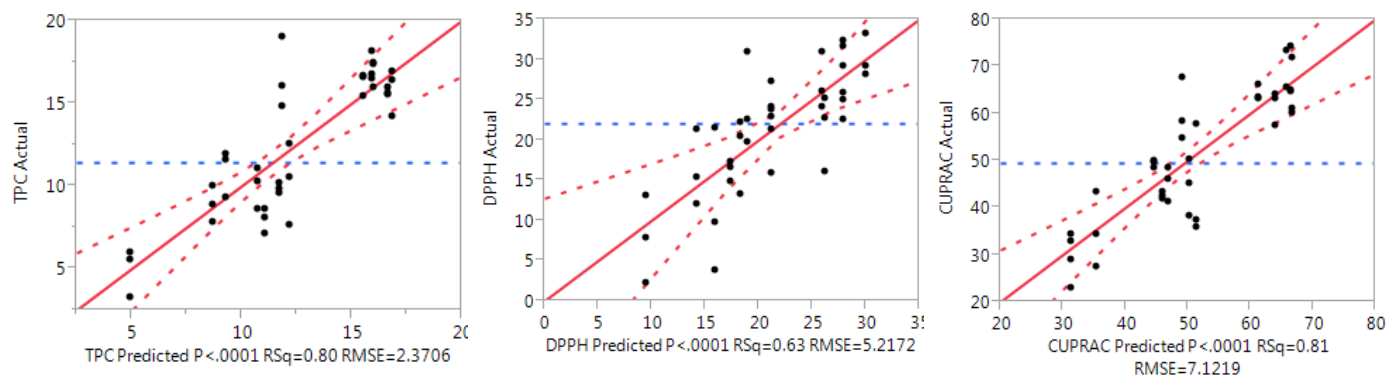


Figure 1. Correlation between the actual and predicted values for TPC, DPPH and CUPRAC of the aqueous olive pomace extract.

Figure 2

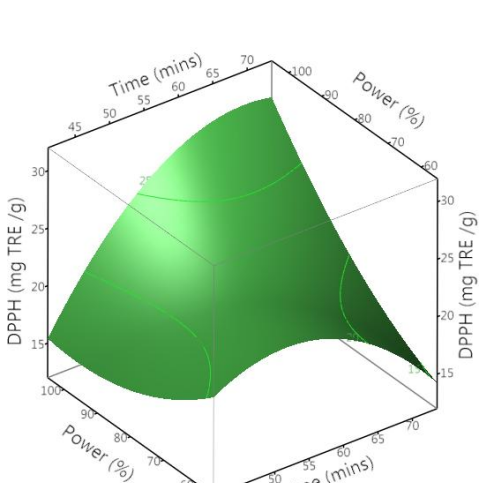
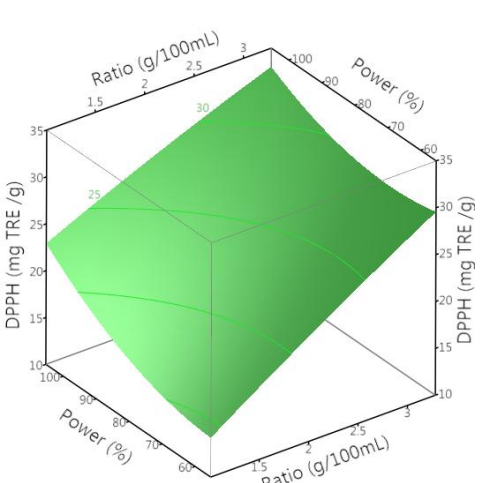
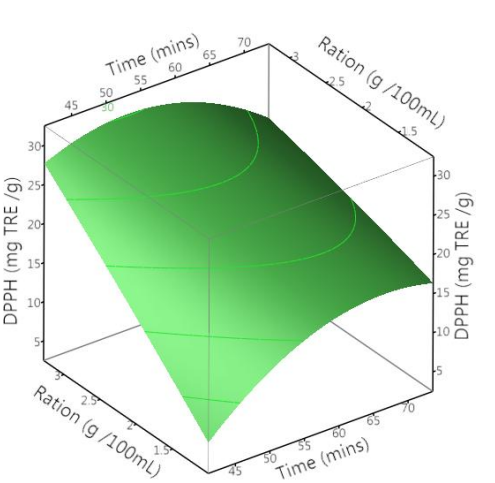
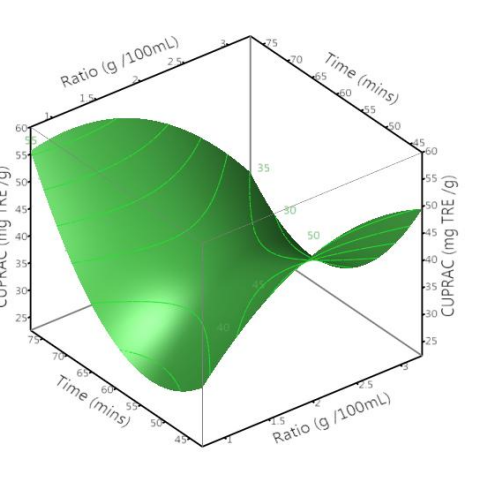
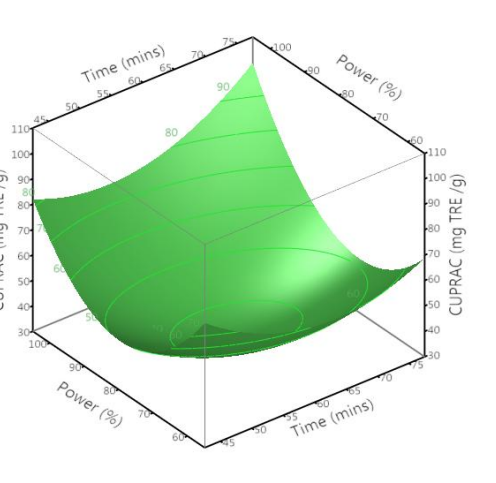
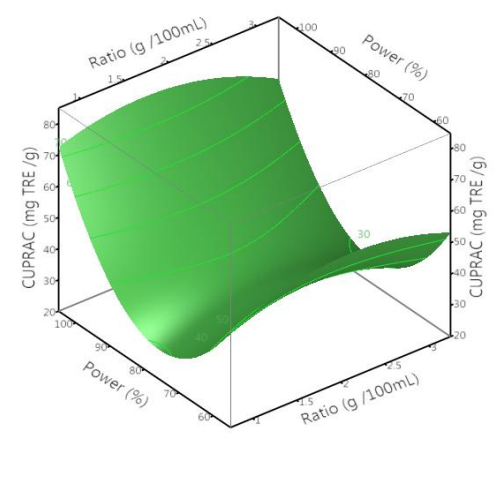
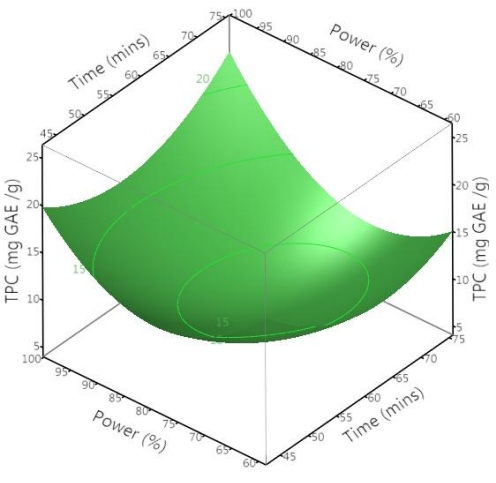
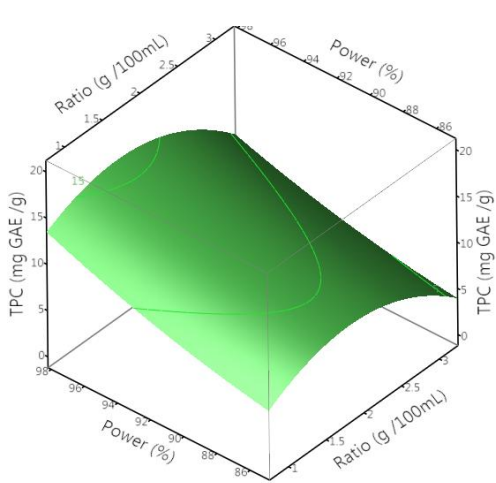
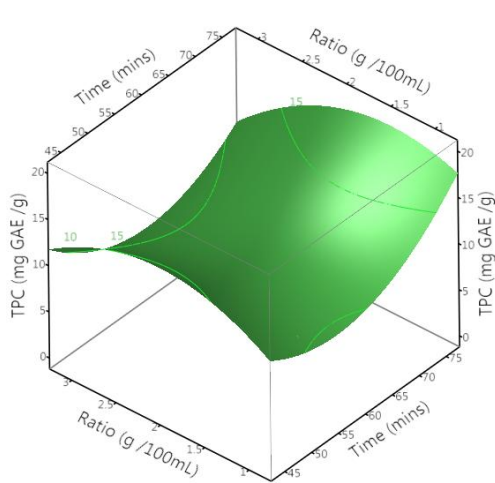


Figure 2. 3D response surface and 2D contour plots for the effect of the test parameters on the total phenolic compounds (TPC) and antioxidant activity (DPPH and CUPRAC) of the aqueous olive pomace extracts.

Figure 3

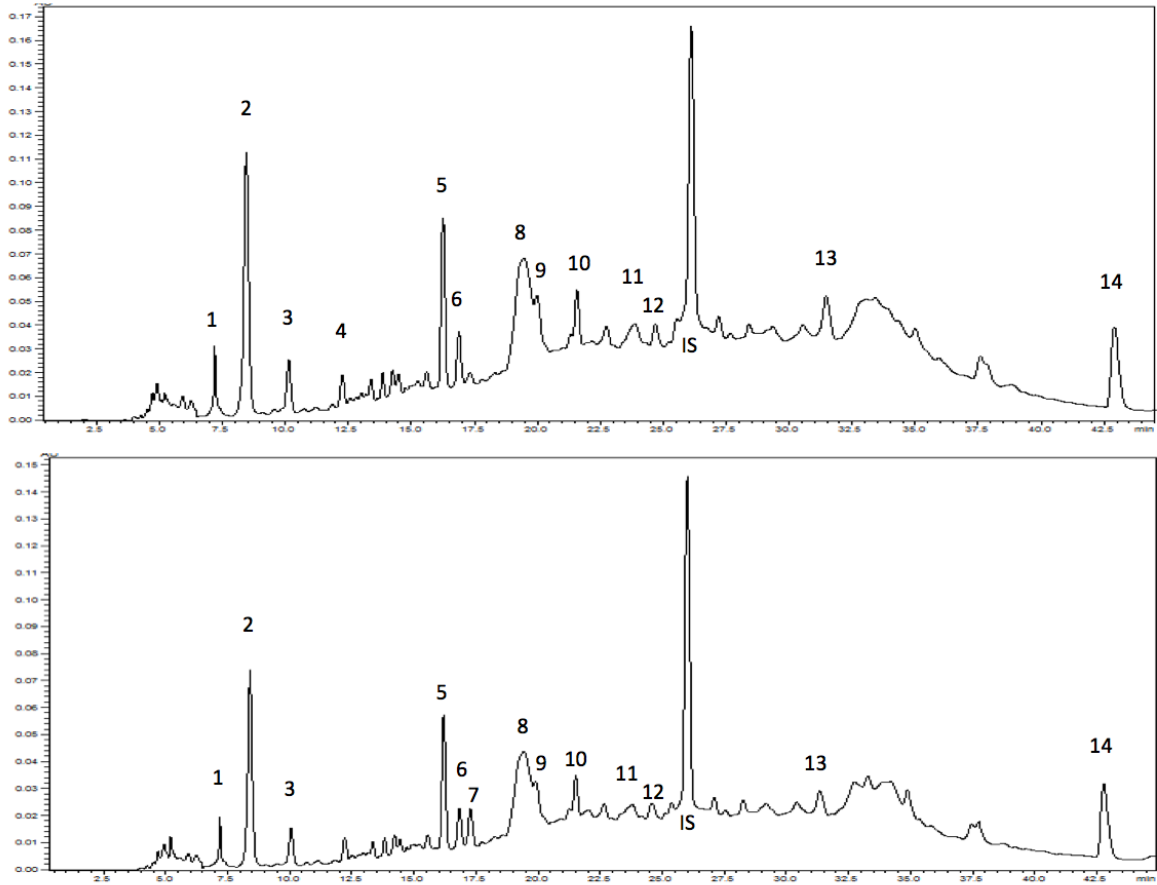


Figure 3. Typical HPLC chromatogram at 254nm of; (Top) optimal UAE extract (Bottom) control extract. The internal standard (IS) was syringic acid.

*Axes on chromatograms are not the same.