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# Modelling and optimization of wet microalgae *Scenedesmus quadricauda* lipid extraction using microwave pre-treatment method and response surface methodology

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Abstract:

The process of extracting lipids from high-moisture *Scenedesmus quadricauda* microalgae biomass disrupted with microwave was examined. The study showed that microwave pre-treatment is effective in algae cell rupture while microwave power was found to be a significant factor to enhance the degree of cell disruption. Though microwave pre-treatment time had some effect, the degree of cell rupture seemed to decrease after a certain pre-treatment time. The total lipid from *Scenedesmus quadricauda sp.* were extracted using a mixture methanol and sulphuric acid as an organic solvent. In addition, it was discovered that microwave pre-treatment enhances the disruption of microalgae cells to attain a high level of lipid yields. Optimal lipid yield obtained in this study was 49% at power 600 W, heating time of 8 min and extraction time of 3.5 h.

Keywords: microalgae, lipid extraction, microwave pre-treatment, modelling, optimization, biodiesel

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## 1. Introduction:

Though algae biofuels are not yet commercial, their economic outlook is promising [1–4]. The obsolete development of lipid extraction from microalgae cells often involves the consumption of a large amount of energy because of microalgae dewatering process [5]. Using microalgae biomass a potential substitute fuel production has increased globally [6], as microalgae represent a renewable energy resource which captures atmospheric carbon dioxide (CO2) photosynthetically and produces lipids that can be converted to biodiesel [7–9]. However, large-scale production of microalgae biomass and energy efficiency is yet to become a sustainable reality.

Fundamental issues are obviously high lipid productivity, energy efficient downstream processes and energy balance in the case of dry route lipid extraction is not positive. According to K. Sander and G. Murthy [10], the minimum net energy input is 3982 MJ for 24 kg of biomass with a lipid content between 30 and 40% (w/w), necessary for the production of 1000 MJ microalgae biodiesel. However, a natural gas dryer requires 3556 kJ/kg water removed which represents 89% of the total energy input. Generally, life-cycle assessment (LCA) studies of biodiesel from microalgae pointed out that the step which requires the most energy input is the biomass drying operation [11]. If the energy input is reduced with an improvement or removal of the drying operation, the net energy balance and cost would be positive [12].

Therefore, lipid recovery by wet extraction is of interest to reduce the energy demand. While Chisti et al. [13] confirm that biorefinery concepts are mainly used to valorise the whole biomass as a strategy to decrease the overall cost of the production, which must not exceed 0.25 dollar/kg to compete for the petroleum. In addition, the energy applied during microwave pre-treatment has been noted to affect microalgae solubilisation, where Dai et al. [14] confirm that increasing microwave pre-treatment power from 400 to 1000 W increases microalgae lipid yield. Qv et al. [15] observed that increasing microwave power from 140 to 560 W increases lipid extraction efficiency. However, most previous studies also reported that further increase in microwave power 700 W decreases microalgae lipid yield. A study conducted by Biller et al. [16] confirms that increasing the microwave power from 25 - 61 Wh/g resulted in increased lipid yield from *Nannochloropsis sp.* biomass from 1.6 to 10%.

Passos et al. [17], noted that increasing the microwave energy from 300-900 W increases microalgae biomass solubilisation. The energy consumed during microwave irradiation pre-treatment depends on the temperature and duration of cell disruption. Some previous studies have studied the effects of energy consumed during microalgae cell disintegration on lipid yield. Balasubramanian et al [18], arrive at a conclusion that 76-77% of the oil from dried *Scenedesmus obliquus sp.* was achievable using microwave radiation with an energy consumption of 60 Wh/g. The high moisture of microalgae growth medium of 99.9% w/w has increasingly become a barrier for the entire production process [19]. Lee et al. [20] confirm that disrupting 100 ml of microalgae cell suspension by microwave with an energy input of 700 W for 5 min, the energy consumed is equivalent to 420 MJ kg1 of dry algal mass. In addition, physical and chemical harvesting techniques such as sedimentation, flocculation, freeze dry and centrifugation can only decrease the quantity of moisture close to 90% (w/w), where further removal of moisture can only be achieved by drying process [19]. The dry process is not energy efficient and cost-effective, as this increases the possibility of making the entire production process not economically efficient. Also, the size of microalgae strains [21], and the existence of rigid cell wall that requires being ruptured [22–24] to enhance lipid extraction, still has significant challenges in microalgae production process. However, the development of production processes and the conversion of algal biomass to biodiesel to achieve cost efficiencies that rival petroleum-based fuels is an ongoing challenge that demands an in-depth understanding of both algal biology and process engineering [25–27]. Also, the high-quality of algal species is essential in determining the amount of lipid produced, an efficient effective method of lipid extraction is of much importance towards commercial biofuel production [28,29]. Subsequently, for lipid extraction process to be successful using microalgae biomass, there is a need for an efficient cell disruption phase that will enhance lipid production. Previous studies have used both mechanical and non-mechanical pre-treatment for microalgae cell rupture[30]. A study conducted by Halim et al. [22] used direct counting and average colony diameter methods to determine the disruption efficacy of many treatments to lyse *Chlorococcum sp.,* these includes; high pressure homogenizer (73.8%), sulphuric acid treatment (33.2%), bead beating (33.2%), and ultrasonic (4.5%). They concluded that high-pressure homogenizer has the highest percentage of cell rupture but is not energy efficient. Lee et al. [31] affirms that bead beating effectively disrupts algae cell more efficiently. A study by Chisti et al. [32] evaluated the use of

mechanical disruption technique using bead beating, HPH with liquid shear, ultrasonic and freeze press, and they concluded that cell rupture is dependent on the microorganism. The outstanding problem about mechanical cell rupture is that they are not energy efficient. For this reason, previous studies have demonstrated that microwave pre-treatment has been effectively used in cell disruption of microalgae cell walls [18,33–35] to enhance lipid production. This method has been applied in numerous areas which includes: chemical synthesis, solvent extraction, and solid state reaction [36]. Other applications includes; catalytic and non-catalytic transesterification processes [37], pyrolysis and hydrothermal liquefaction of microalgae for biofuel production[38].

Other studies that applied microwave irradiation pre-treatment on different biomass material to produce biogas includes [17,39–42]. In addition, Refaat et al. [43], applied microwave pre-treatment using sunflower and achieved 5.96% of lipid, Chen et al. [44] uses waste cooking oil and produces 38.31% of lipid and Cheng et al. [45] also applied microwave pre-treatment using *Nannochloropsis Oceanica sp*. and recorded 38.46% of lipid yields. Balasubramanian et al. [18] added that increasing reaction time from 10 and 20 min using microwave pre-treatment on *Scenesdesmus obliquus* sp. enhances lipid yield from 10% to 22%. Thus, microwave energy can play an important role in microalgae cell pre-treatment to enhance biofuel production. Also, microwave time plays a significant role during microalgae cell disruption, which determines the recovery efficiency of the lipids present in microalgae biomass [46]. Menendez et al. [47] observed the effect of increasing microwave pre-treatment time from 10 -20 mins using *Nannochloropsis gaditana* and achieved a lipid yield of 29-40%. Balasubramanian et al. [18] affirmed that increasing the microwave heating time from 10-20 mins resulted in an increased in lipid yield from 10-22% using Scendesmus obliquss after pre-treatment. while Dai et al. [14] concluded that that increased in microwave extraction time from 10 to 40 min resulted in increased microalgae lipid recovery 14 to 18%. However, all the research works mentioned above used dry and different biomass material for lipid production, at present no study has used microwave pre-treatment on *Scenesdemus quadricauda* to enhance lipid extraction. Considering the energy and equipment cost related to drying and dewatering microalgae cells, it would be cost-effective if wet microalgae cells can be used directly for biofuel production after pre-treatment. Also, the extraction of lipids from dried microalgae cells incurs a large amount of energy during dewatering process. To

improve this situation, some research studies has focused on an alternative approach for the lipid extraction using wet microalgae, as discussed in [31,36,48–50].

Therefore, the objectives of the study include; (a) Modelling and optimization microwave pre-treatment parameters using response surface method after lipid extraction. (b) Performing numerical optimization to find the optimal combination of microwave power and time and reaction time that could maximize the % of lipid yield, which is cost efficient as compared to other previous works.

## 2. Materials and Methods:

### 2.1. Microalgae Cultivation

Microalgae strain (*Scenesdemus quadricauda*) were purchase from Sciento-Manchester. 50 ml of each algae sample was kept in freezer at a temperature of 0 to 4°C to maintain a constant growth rate. The sample was cultured within the School of Engineering, University of the West Scotland (UK), in a 4-liter flask each after sterilization with distilled water at a temperature of 60°C for 4 hours and 3 g of the unicellular culture medium (K10) was bought from Sciento (Manchester, UK) was then added. The chemical composition of K10 unicellular medium includes; Sodium nitrate, Magnesium sulphate, Dipotassium hydrogen orthophosphate, Calcium chloride, Ammonium chloride and Trace elements with weight (%) of 62, 16, 15, 4 ,3 and <1 respectively). The flask was vigorously hand shake twice each day to enhance appropriate circulation of the nutrients during cultivation period. Room temperature of 15°C to 25°C was maintained throughout the culture period. A spectrophotometer at a wave length of 600 nm was used to determine the initial cell concentration before and at the end of culture period; which has the value of $1.815 \times 10^8$ cell/ml and $7.7637 \times 10^{16}$ cell/ml. After 20 days, the cultivation process was completed.

### 2.2. Microwave Pre-treatment

500 ml sample of the standard culture were subjected to microwave pre-treatment using a round bottom open glass. The samples were pre-treated at different microwave power of 600 W, 390 W and 180 W and time between 8, 5 and 2 minutes, until each pre-treatment phase is completed. The pre-treatment was performed using a stainless-steel microwave oven

149 (Bosch BOSHMT75M451B, 800 W, 5 power levels and 60 min timer). All the experiments
150 were run in duplicate and the average results are presented in this paper.

151 2.3. Extraction Procedure:

152 Initially, 500 ml of wet algae sample were pre-treated using a conventional microwave
153 according to pre-determine microwave power and time. The two parameters were selected
154 based on previous research studies to give a distinct percentage of cell disruption [19]. A
155 500 ml of each pre-treated sample were placed in a flask by adding 500 $cm^3$ of methanol and
156 10 ml of sulphuric acid. Anti-bump granules were added to the flask and reflux at each
157 selected time of reaction. After the refluxing, the sample was extracted using 3 x 150 ml and
158 washed with 5% of sodium bicarbonate solution. The reflux process was repeated for 14
159 different experimental conditions with different extraction times (3, 3.5 and 4 h respectively).
160 The solvent used was evaporated using a steam bath to obtain the liquid extract.

161 2.4. Design of Experiments:

162 The experimental modelling was designed for 3 input parameters with three levels.
163 Microwave power varies from 180 to 600 W, microwave time between 2 to 8 min and
164 reaction time between 3 to 4 hrs. The output response was % of lipid recovered after each
165 extraction time. Both the process parameter and output response results are indicated in
166 Table 2. A Box-Behken Design with three factors was selected for design of experiments.
167 Fourteen experiments were determined by DOE, statistical analysis as well as the provision
168 of extensive graphs that showcase the relationship between the input parameters and the
169 output responses [51,52]. The process parameters selected was microwave power, time and
170 extraction time. The response was the % of lipid produced per each 500-ml sample produced.
171 RSM is considered by high adherence to the experimental data describing the reality of what
172 was studied [53]. Moreover, RSM methods are able to exhibit the factor contributions from
173 the coefficients in the regression model to identify the insignificant factors and thereby,
174 reduce the complexity of the problem[54]. Table 1 summarises the three levels and ranges of
175 process parameters used in the design, while Table 2 shows the experimental conditions and
176 amount of lipid recovered using Box-Behken design.

177 Table 1. Process variables and their units, levels used in the Experimental Design.

| Variable | Units | Levels | | |
|---|---|---|---|---|
| | | -1 | 0 | 1 |
| Microwave Power | W | 180 | 390 | 600 |
| Time | min | 2 | 5 | 8 |
| Extraction Time | h | 3 | 3.5 | 4 |

178

179 Table 2. Box-Behken Design experimental design matrix showing the effects of process
180 parameter on the output response (% recovered lipids).

| | Input | | | Results |
|---|---|---|---|---|
| | Factor 1 | Factor 2 | Factor 3 | Response |
| Run | A: Power | B: Heating Times | C: Extraction Time | % Recovered lipid |
| | W | min | h | % |
| 1 | 180 | 5 | 3 | 14.01 |
| 2 | 180 | 2 | 3.5 | 14.44 |
| 3 | 180 | 8 | 3.5 | 10.83 |
| 4 | 180 | 5 | 4 | 18.86 |
| 5 | 390 | 2 | 3 | 18.87 |
| 6 | 390 | 8 | 3 | 18.87 |
| 7 | 390 | 5 | 3.5 | 32.43 |
| 8 | 390 | 5 | 3.5 | 11.68 |
| 9 | 390 | 5 | 3.5 | 25.46 |
| 10 | 390 | 2 | 4 | 14.44 |
| 11 | 390 | 8 | 4 | 37.84 |
| 12 | 600 | 5 | 3 | 32.43 |
| 13 | 600 | 2 | 3.5 | 18.69 |
| 14 | 600 | 8 | 3.5 | 48.65 |
| 15 | 600 | 5 | 4 | 25.45 |

181

182 2.5. Analysis method

The experimental data analysis was performed using Design Expert software version 10, which predicts the optimal condition. The quadratic polynomial model used for response surface regression procedure for this work is shown in Eq 1. Also, RSM consist of a group of mathematical model and statistical techniques used in the development of an adequate functional relationship between a response of interest, y, and several associated control or input parameters denoted by $\times_1 \ldots \ldots \times_2 \ldots \ldots \ldots \times_k$. Hence, the second order polynomial equation is shown in Eq. (1), this is used to describe the true functional relationship between the input parameters and the output response.

$$Y = b_0 + \sum b_i X_I + \sum b_{ii} X_{ii}^2 + \sum b_{ij} X_i X_j \quad (1)$$

Where Y is the amount of lipid produced (Output Response), $b_o$ is the coefficient of the equation, $X_i$ and $X_j$ are the coded levels variables. X is the independent parameter and $b_i$, $b_{ii}$ and $b_{ij}$ are the intercept, linear quadratic and interaction regression coefficients respectively. The statistical significance of the model and the process parameters were assessed by analysis of variance (ANOVA), while the quality of the model was determined by the determination coefficient($R^2$). The ANOVA table for the response surface quadratic model on % of recovered lipid is shown in Table 3.

Table 3. ANOVA for response surface quadratic model.

| Source | Sum of Squares | df | Mean Square | F- Value | p-value |
|---|---|---|---|---|---|
| Model | 1344.77 | 7 | 192.11 | 4.54 | 0.0320 |
| A-mw power | 562.47 | 1 | 562.47 | 13.28 | 0.0082 |
| B-mw time | 309.38 | 1 | 309.38 | 7.31 | 0.0305 |
| C-reaction time | 19.25 | 1 | 19.25 | 0.45 | 0.5218 |
| AB | 281.74 | 1 | 281.74 | 6.65 | 0.0365 |
| AC | 34.99 | 1 | 34.99 | 0.83 | 0.3936 |
| BC | 136.89 | 1 | 136.89 | 3.23 | 0.1152 |
| $A^2$ | 0.055 | 1 | 0.055 | $1.3 \cdot 10^{-3}$ | 0.9722 |
| Residual | 296.45 | 7 | 42.35 | | |
| Lack of Fit | 73.44 | 5 | 14.69 | 0.13 | 0.9695 |
| Pure Error | 223.01 | 2 | 111.51 | | |
| Cor Total | 1641.22 | 14 | | | |

$R^2 = 0.8194$ Pred $R^2 = 0.4903$ Adj $R^2 = 0.6387$

## 3. Results and Discussion:

### 3.1. Development of a regression model.

The 15-experimental results for *Seneesdemus quadricauda* are shown in Table 2. The percentage of recovered lipid ranged from 14.01% to 48.65%. The final mathematical model associated with the response in terms of actual factors is shown in Eq. 2, while the ANOVA test is indicated in Table 3.

$$\% RL = 42.20 + 0.07A - 16.77B - 5.41C + 0.01AB - 0.03AC + 3.90BC + 2.75 \times 10^{-6}A^2 \quad (2)$$

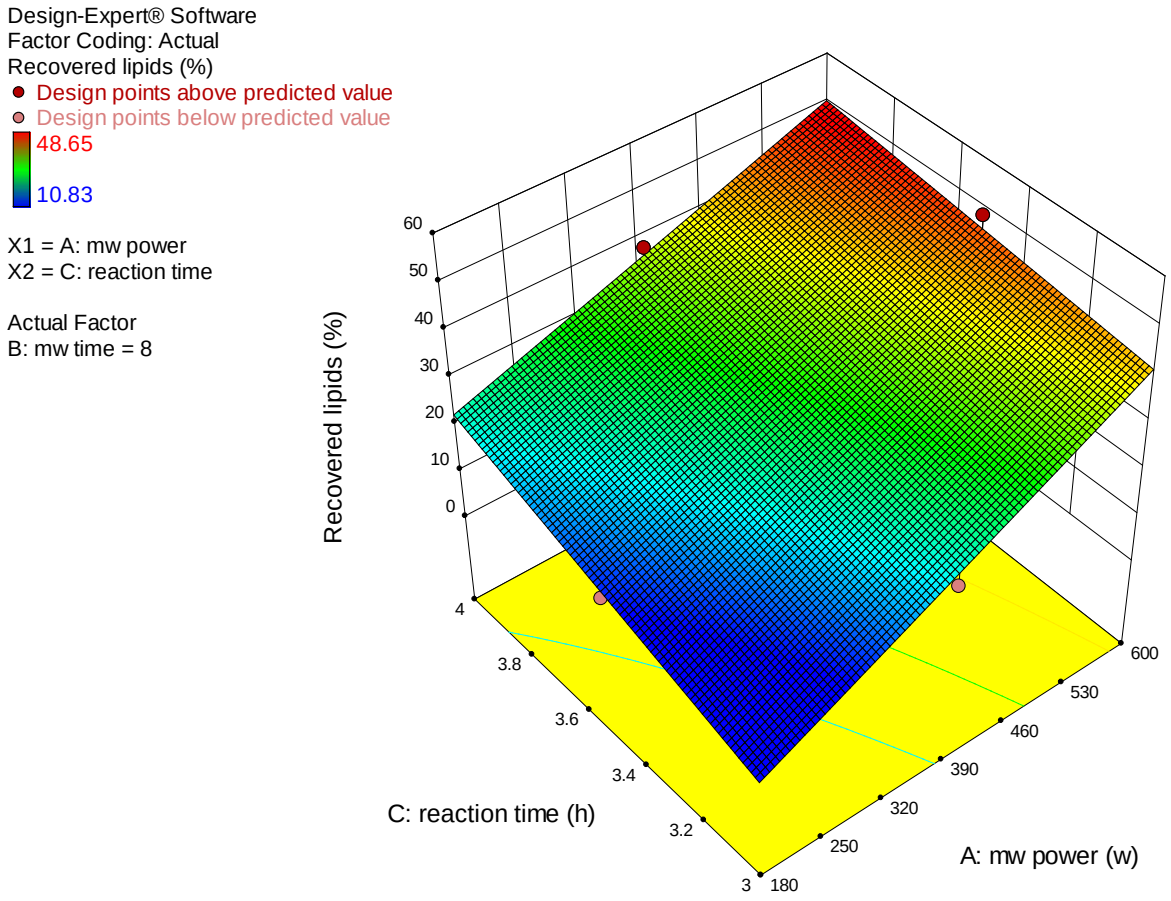
where RL: Recovered lipids A- microwave power, B-microwave time, C-reaction time as indicated in Table 3.

A variation less than 0.2 between adjusted-$R^2 = 0.6387$ and Predicted-$R^2 = 0.4903$, indicated that the adopted model is adequate. The entire adequacy measures are less than 0.2, which are in reasonable agreement and significantly shows adequate model [55,56], because the statistical analysis as considered by the *Design Expert*, it indicates that any value equal less

than 0.2 are considered when determining the adequacy measures of adjusted-$R^2$ and Predicted-$R^2$. Where lack of Fit F-value of 0.13 implied that lack of fit was not significant relative to the pure error (Table 2), this was tested to know if the Prob >F of the lack of fit exceeds the level of significance as shown in table 3. Also, in Response surface methodology (p-value) of lack fit if >0.05 (not significant) signifies that the model fits well and there is no significant effect on parameters on output response. Hence, the term adjusted R-squared as indicated in the ANOVA table 3. compares the explanatory power of regression models that contain different numbers of predictors, also it is a modified version of R-squared that has been adjusted for the number of predictors in the model. They increase only if the new term improves the model more than would be expected by chance. While predicted R-squared indicates how good a regression model predicts response for new observation, it determines when the model fits the original data but less capable of providing valid predictions for new observation.

3.2. Effects of interaction between parameters using response surface methodology plots.

The response surface plot (Fig 1) obtained from the model shows the effect of microwave power and reaction time in the % of recovered lipids. For a fixed microwave time of 8 min and extraction time 4 hrs, increasing the power from 180 to 600 W, the % of lipid-recovered increases by 150% respectively. For a maximum pre-treatment conditions of 600 W and 8 min, the % of recovered lipids increased by 25% by increasing the reaction time from 3 to 4 h. The effect of pre-treatment time is shown in Fig 2, for a fixed reaction time of 3.5 hrs and a microwave power of 600 W, an increase of 200% is achieved by increasing the pre-treatment time from 2 to 8 min. If the microwave power is set at the lowest value of 180 W, for the same variation in pre-treatment time, the increased obtained is 50%. This shows that pre-treatment time has a higher effect on high microwave power. Combining high microwave power and time, the highest % of recovered lipids are achieved.




249

250 Figure 1. 3D response surface plot for % of recovered lipid using microwave power and time.

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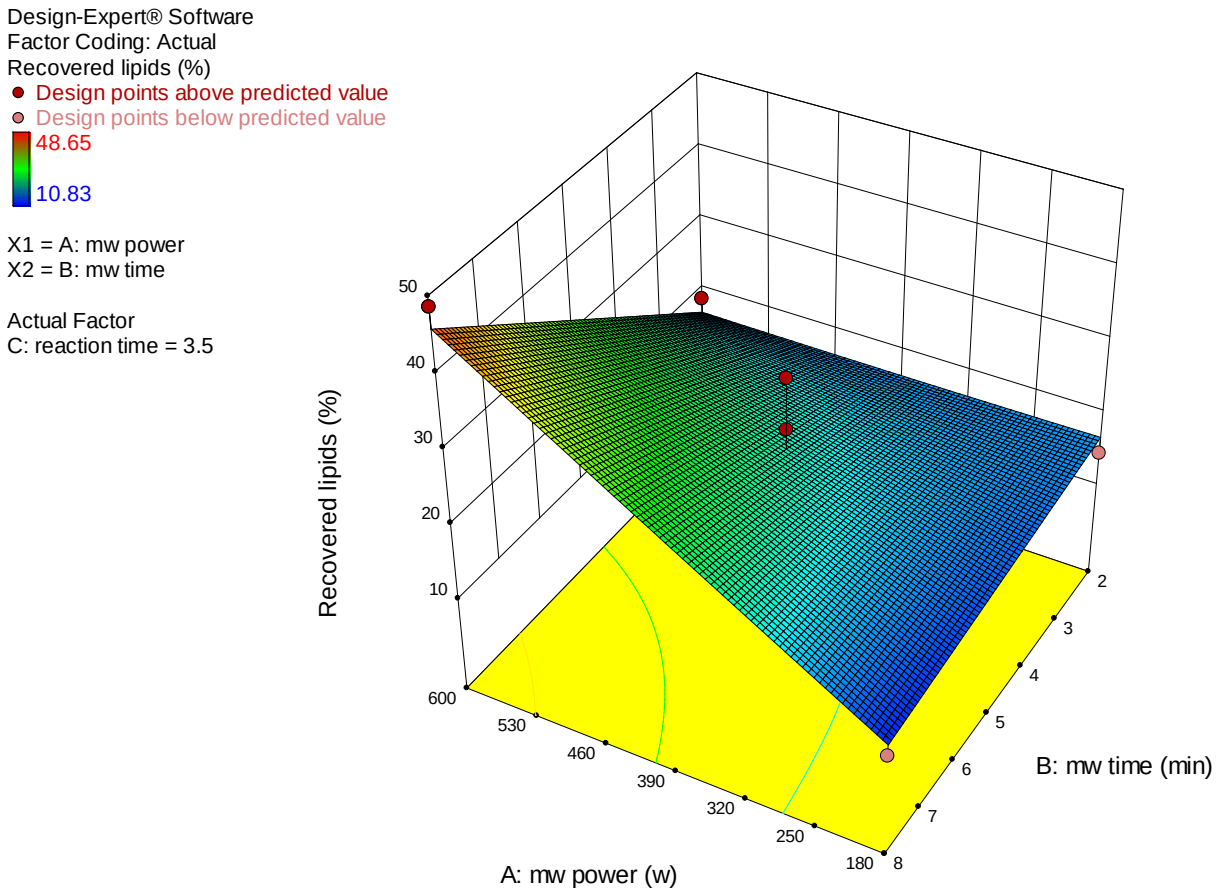


Figure 2. 3D response surface plot for % of lipid recovered using microwave power and reaction time.

This proves that at a pre-treatment power of 600 W for 8 min the algae cells have been disrupted to enhance the lipid extraction. This fact correlates with the study conducted by [33,34,41,46,57–62] that using a high microwave power increases lipid efficiency. Though a decrease in both microwave power and time reduces lipid efficiency, this may be because of some of the algae cells remain undisrupted which inhibit the rate of lipid extraction. The reaction time has a significant effect on the % of lipid recovered. Generally, extended pre-treatment time provides an enhanced exposure of microalgae mixture to microwave effect, which improves a better yield of lipid. Decreasing the exposure time seems not to provide enough cell-disruption degree to achieve high % of recovered lipids. For this reason, one can assume that a low pre-treatment time, the algae cell remains intact which may lead to a low lipid yield (Table 2). The reaction time around 3.5 to 4 h and heating time of 8 min seems to

be satisfactory for complete extraction under microwave pre-treatment. Thus, the efficiency of lipid extraction increased due to high cell-disruption after microwave pre-treatment. Also, an import fact to note for future research is that more work should focus on the effects/benefits of harvesting microalgae cells as summarized by the [63]. In addition, few reviews studied the effect of microwave pre-treatment to enhance lipid extraction efficiency for biofuel production. Cheng et al. [45] observed the effect of pre-treating *Nannochloropsis Oceania sp*. using microwave irradiation at a frequency of 245 MHz and a power increase from 635-1022 W for 15 mins pre-treatment. It was recorded a 38.46% of lipid yields. This present shows that lipid production was achieved at a higher microwave energy and pre-treatment time. This result agreed well with [14,20,64], who realized that increasing in microwave power have a significant effect on the production of lipid using different microalgae cells. A different study conducted by Cheng et al. [65] noticed the effect of microwave pre-treatment at a frequency of 2.45 GHz, a reduction in power from 600-500 W for 5-60 mins on (*Chlorella pyrenoidosa).* The author realized a 15% of lipid yield after decreasing the microwave power to 500 W with an increase in pre-treatment time. A similar result obtained by [14,47,66] agrees that increasing microwave pre-treatment time increases lipid yield production. At the end of the microwave pre-treatments, the lipid yield was 10-22%, 29-40% and 14-18% respectively. In this research work, a short microwave pre-treatment time of 8 mins power of 600 W increase the lipid extraction rate to 49% using wet microalgae cell (*Scenedesmus quadricauda sp.)* which is higher than all the above results as discussed.

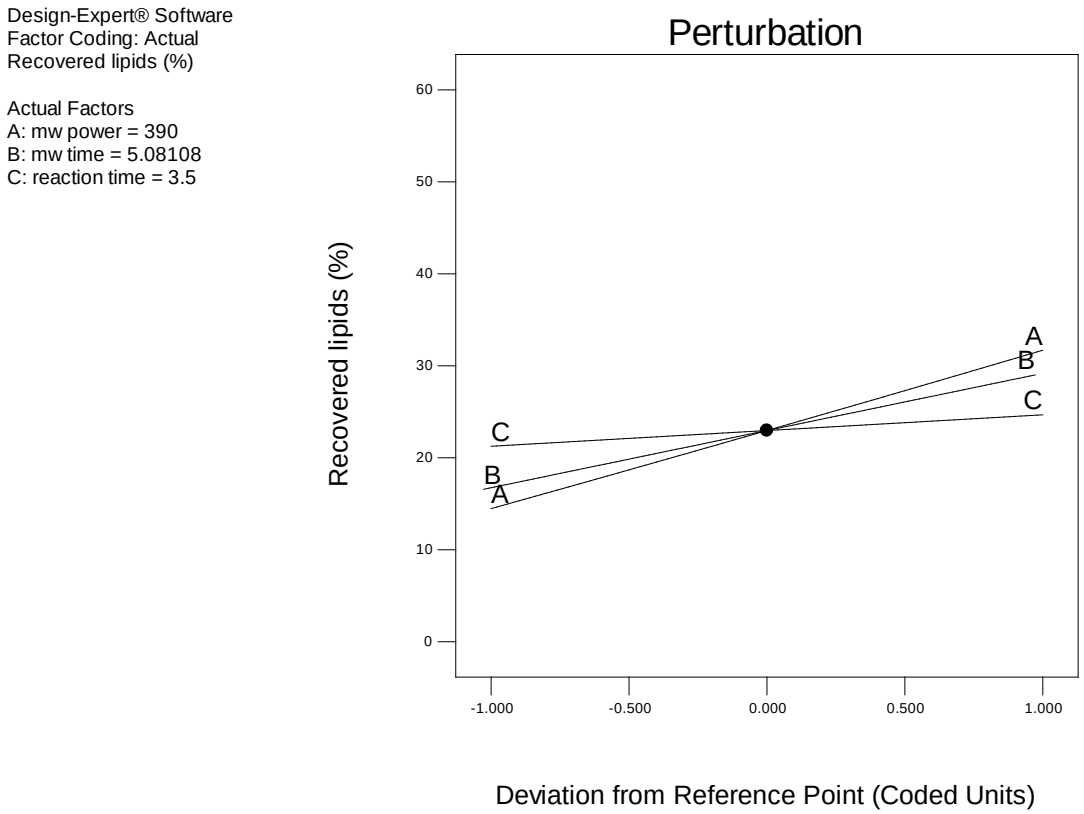


Figure 3. Perturbation plot for % of recovered lipid.

The perturbation plot in Fig. 3 clearly shows how % of recovered lipid is affected by the input parameters microwave power and time and reaction time. Increasing the microwave power and heating time, the % of lipid recovered will increase linearly. Reaction time has little effect on lipid recovery as shown by the quasi-horizontal line C in Fig 3.

### 3.3. Optimization of lipid recovered

With respect to the model as represented in in Eq. 2, above, which systematically gives a concise description of the effects of input parameters to the output response (% of lipid recovered), optimization was performed using Design Expert software version 10. Hence, optimization principle is based on the combination of final product maximization (productivity). In this case, optimization simply means maximizing operational efficiency to improve output efficiency. The aim of the optimization is to find the optimal combination of microwave power and times that could maximize the % yield of lipid yield. The % of lipid

recovered was maximized with level 5 and microwave power was minimized with level 3. An optimum % of recovered lipid of 41.94 was obtained at microwave time of 8 min, microwave power of 473 W and reaction time of 4 h. The optimization plots (Fig 4 and 5) gives a concise description of the optimal process parameters by means of visual observation. The yellow region in the optimization plot signifies the values that meet the planned standards truly established by the curves agree with the standard of the optimization criteria. The plots clearly established that the optimum conditions for a maximized % of recovered lipids are above 350 W and 4 min of microwave pre-treatment.

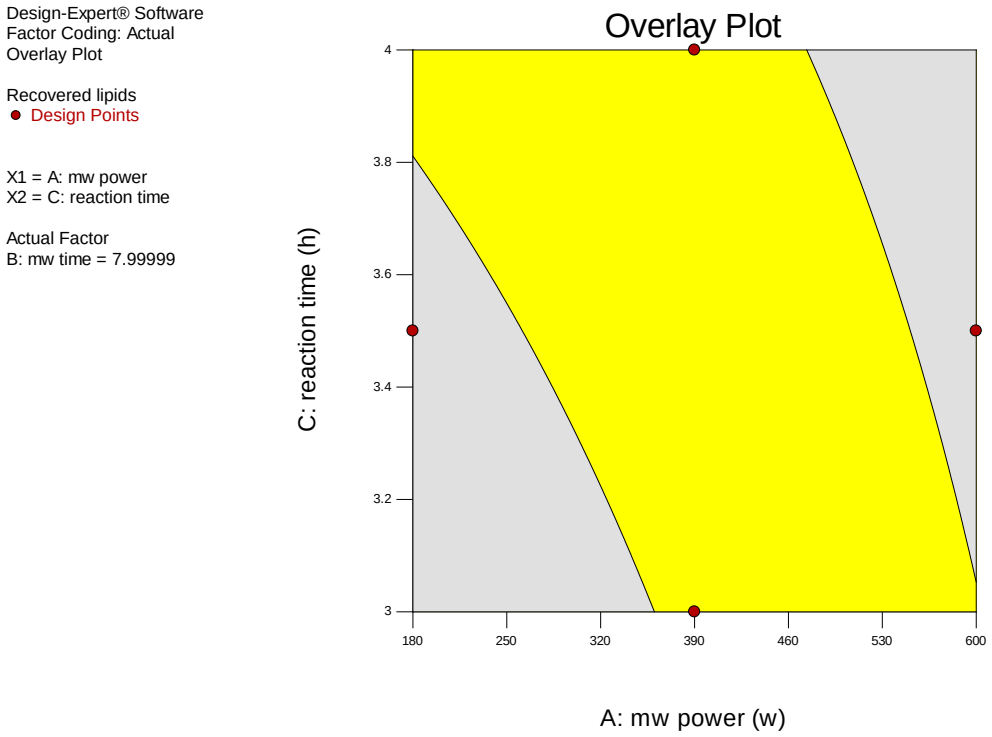


Figure 4. Graphical optimization showing the effect of reaction time and microwave power.

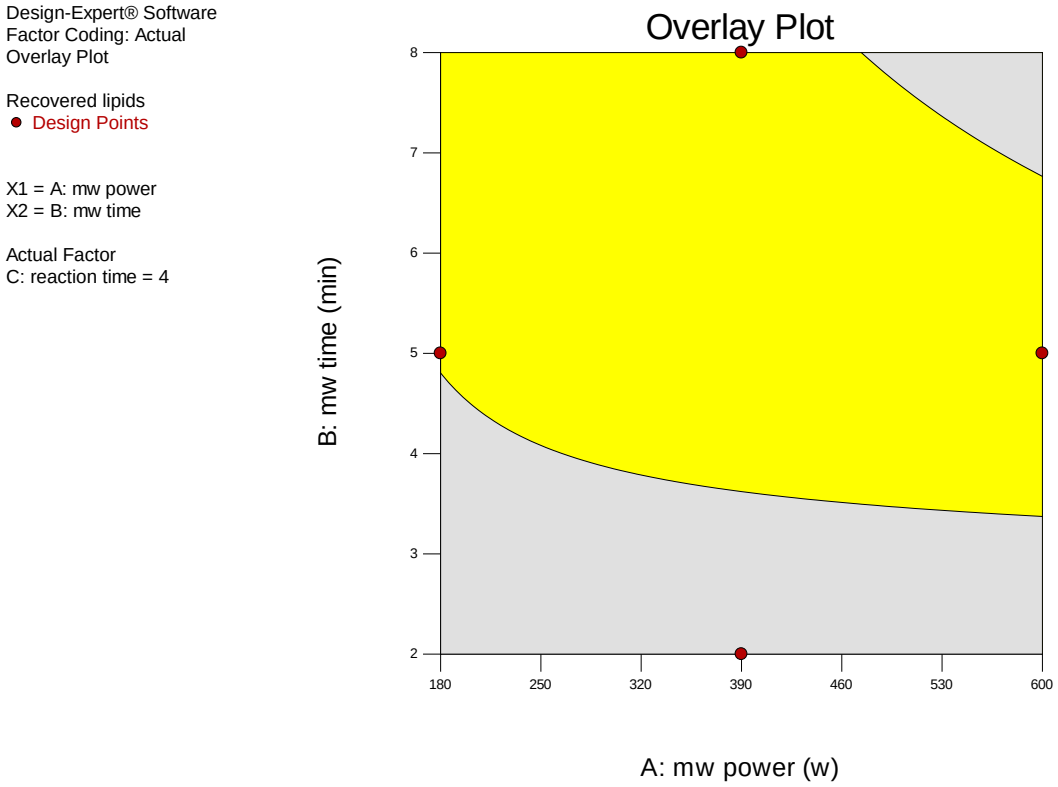


Figure 5. Graphical optimization showing the effect of microwave time and power.

To confirm the viability of this method, the optimum point of the RSM (section 3.3) was compared with a commercial sample of biodiesel from a petrol station (Biodiesel 80:20 mix).

| Analytes | Commercial Sample (µg/ml) | Optimum sample (µg/ml) |
|---|---|---|
| methyl myristate - C14 | 0.00 | 154.73 |
| methyl palmitate - C16 | 110.50 | 268.12 |
| methyl stearate - C18 | 102.23 | 27.92 |
| methyl linoleate - C18:2 | 171.00 | 8.38 |
| methyl arachidate - C20 | 117.45 | 10.21 |
| methyl eicosate - C20:1 | 515.20 | 21.22 |
| methyl eicosadienoate - C20:2 | 359.45 | 14.46 |
| methyl erucate - C22:1 | 13.11 | 4.91 |

The result clearly established the presence of individual FAME's that are required to accurately identify the sample as viable for biofuel production. From the table 4, the concentration of FAME sample was found to be 268.12µg/ml higher in methyl palmitate - C16 as when compared with the commercial biodiesel (80:20 mix), methyl myristate - C14 was not present in the commercial biodiesel as it was present in FAME extract with a concentration of 154.73µg/ml. It can be concluded that this method has a significant contribution towards microalgae biofuel industry.

## 4. Conclusion

Pre-treating algae biomass with microwave for 600 W, from 2 to 8 min enhances the % of recovered lipid to 49%. In addition, the reaction time from 3.5 to 4 hrs seems to be satisfactory for complete extraction under microwave pre-treatment for lipid extraction efficiency. An optimization study was accomplished to reduce the operating cost and pre-treatment time to maximize the lipid production efficiency. The basic aim is to maximize the % of lipid production while minimizing the microwave pre-treatment time. An optimum % lipid yield of 41.94 was obtained at a microwave time 8 min, a reaction time of 4 hrs and power 473 W. The highest lipid yield reported after pre-treatment as when compared with results obtained from literature was reviewed in this research study. As cheng et al. [45] reported a lipid extraction using a dry algae cell to achieve 38.46% lipid after pre-treatment, while Menendez et al. [47] achieve 29-40% of lipids by increasing the time to 20 mins. Other results as reported in the literature above has a low value of lipid yield even with a high pre-treatment time as compared to this present study. This idea concludes the fact that using a wet microalgae biomass shows a desirable value and lipid profile as a potential feedstock for biodiesel production.

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