

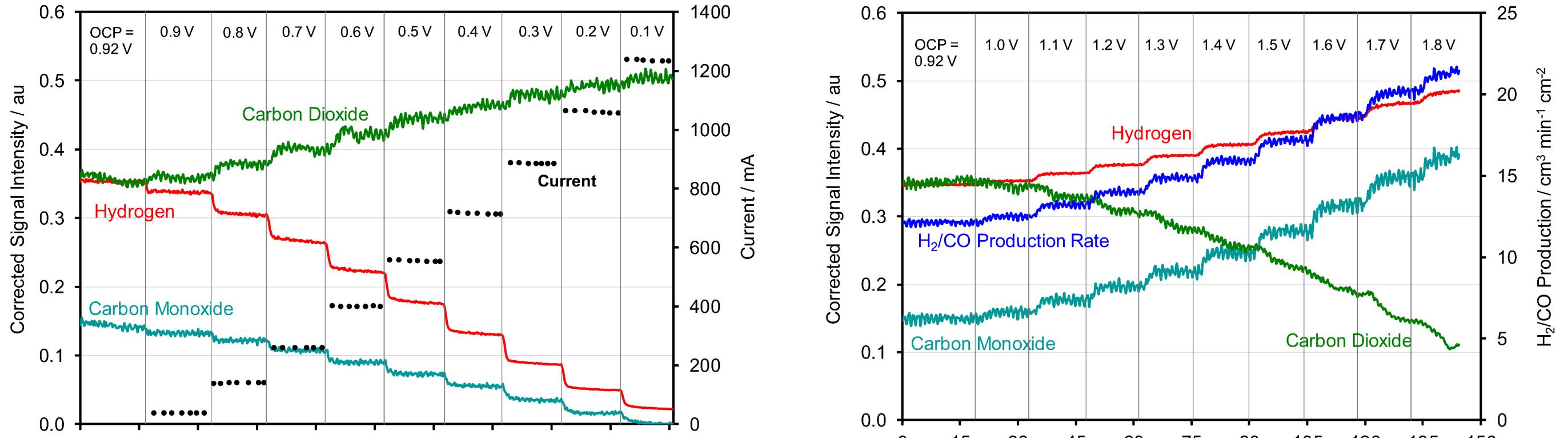
## Utilisation of renewable feedstocks in solid oxide fuel cell technology: biohydrogen

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**Introduction.** Biologically produced mixtures of  $H_2$  and  $CO_2$  (biohydrogen) from processes such as dark fermentation or photo-fermentation are versatile feedstocks which can potentially be utilised in solid oxide fuel cell (SOFC) technology. SOFCs are high temperature (500 – 1000 °C) electrochemical energy conversion devices made with ceramic and metallic materials. They are highly efficient, operate silently and can be sized from 1 kW<sub>e</sub> to 1 MW<sub>e</sub> upwards due to their modular and scalable design.

They can utilise hydrogen or carbon-based feedstocks either in fuel cell mode to produce electrical power and heat, or electrolysis mode to produce useful chemicals such as synthesis gas ( $H_2 + CO$ ). This work investigates the performance and products of a solid oxide fuel cell operating on biohydrogen in both fuel cell mode and electrolysis mode.

**Results.** On entry into the SOFC, approx. 30% of biohydrogen is converted into CO and H<sub>2</sub>O via the reverse water-gas shift (RWGS) reaction (see Figs. 1 and 2):  $H_2 + CO_2 \rightleftharpoons CO + H_2O$ 



0 15 30 45 60 75 90 105 120 135 150 Time / m

**Figure 1.** Utilisation of biohydrogen in SOFC in fuel cell mode. The emissions and current output of the cell are shown.

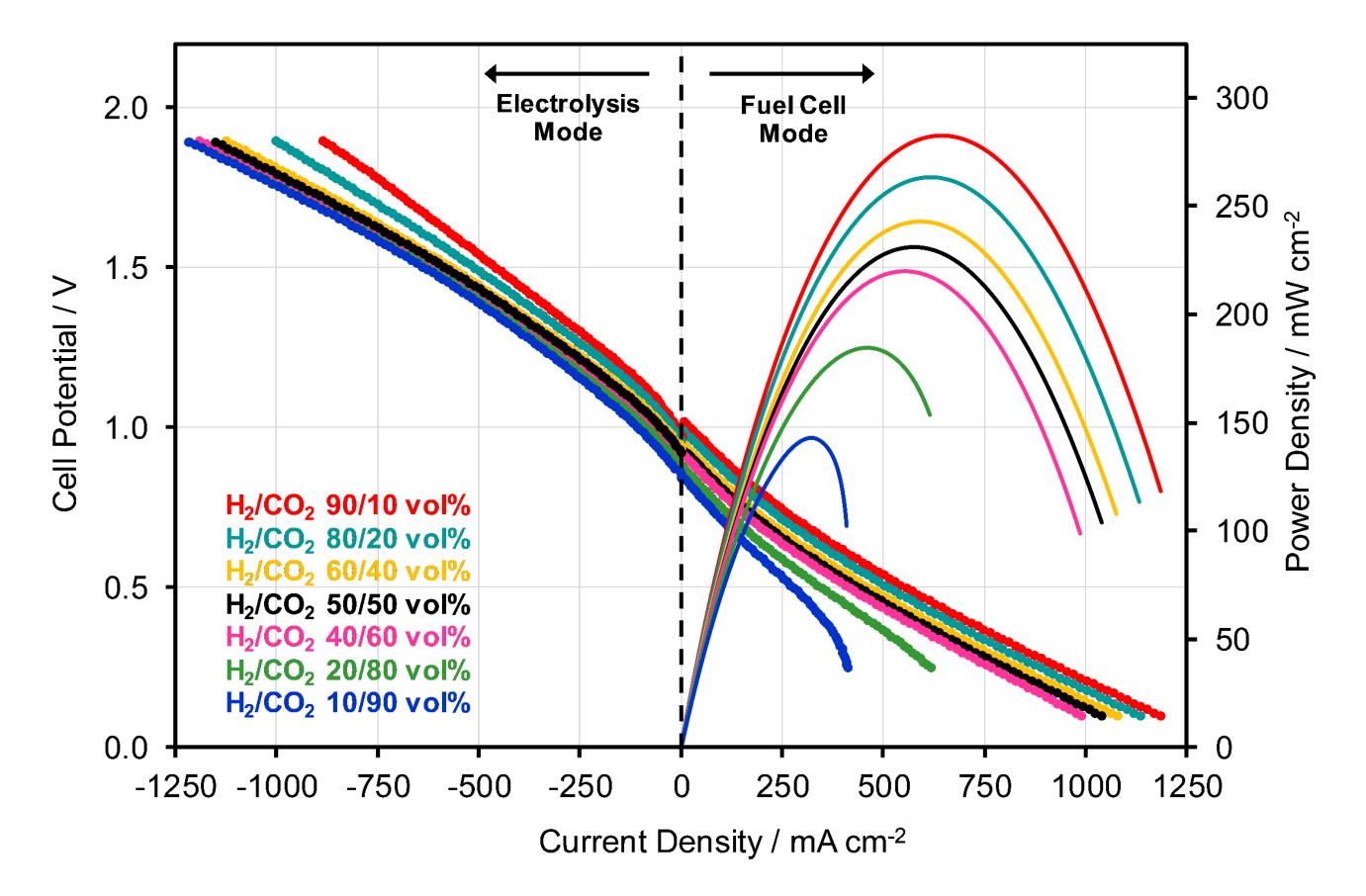
In fuel cell mode (see Fig. 1), the SOFC converts  $H_2$  into **electrical power and heat**. CO is converted via reaction with  $H_2O$  and does not contribute to power production. When the cell is operated at high fuel utilisation efficiency (at 0.1 V in Fig. 1), emissions of CO are minimal.

In electrolysis mode (see Fig. 2), the SOFC converts  $CO_2$  into CO, yielding **synthesis gas**. The H<sub>2</sub>/CO ratio can easily be controlled in the range 1.2-2.3 by adjusting the operating voltage of the cell.

Biohydrogen is inherently variable; however, Fig. 3 shows the electrochemical performance of the cell is not significantly affected by fuel variability provided the  $H_2$  content of biohydrogen stays within the range 40-60 vol%.

## 0 15 30 45 60 75 90 105 120 135 150 Time / m

**Figure 2.** Utilisation of biohydrogen in SOFC in electrolysis mode. The syngas production rate and output gases are shown.



**Conclusions.** Biohydrogen is a useful and renewable feedstock which can be utilised in SOFC technology to yield useful energy and chemical products. Crucially, the results show that  $CO_2$  scrubbing is not required for good SOFC performance. Fuel conversion takes place via a complex interplay that exists between the fuel cell reactions and the RWGS reaction.

**Figure 3.** The effect of fuel variability on the I-V and power curves of an SOFC operating on biohydrogen. Data are shown for the cell operating on biohydrogen mixtures containing 10-90 vol%  $H_2$ .

**Further reading.** Laycock CJ, Panagi K, Reed JP, Guwy AJ, *The importance of fuel variability on the performance of solid oxide cells operating on*  $H_2/CO_2$  *mixtures from biohydrogen processes*, Int J Hydrogen Energy 2018 **34**;8972-82.

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