

# Electrokinetic flow in a pH-regulated, cylindrical nanochannel containing multiple ionic species

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**Abstract** Considering the wide applications of the electrokinetic flow regulated by pH, we model the flow of an electrolyte solution containing multiple ionic species in a charge-regulated cylindrical nanochannel. This extends previous analyses, where only two kinds of ionic species are usually considered, and a charged surface assumed to maintain at either constant potential or constant charge density, to a case closer to reality. Adopting a fused silica channel containing an aqueous NaCl background salt solution with its pH adjusted by HCl and NaOH as an example, we show that if the density of the functional groups on the channel surface increases (decreases), it approaches a constant potential (charge density) surface; if that density is low, the channel behavior is similar to that of a constant charge density channel at high salt concentration and large channel radius. Several interesting results are observed, for example, the volumetric flow rate of a small channel has a local maximum as salt concentration varies, which is not seen in a constant potential or charge density channel.

**Keywords** Electrokinetic flow · pH-regulated cylindrical nanochannel · Multiple ionic species

## 1 Introduction

Electrokinetic flow has been applied extensively in separation devices, micropumps, and biochemomedical analyses (Daiguji et al. 2004a, b; Mei et al. 2008; Karenga and El Rassi 2010; Karnik et al. 2005; Wang et al. 2009). The fast advances in micro- and nano-scaled channel (Gasparac et al. 2004; Tas et al. 2002; Campbell et al. 2004; Mao and Han 2005) and pore (Li et al. 2001; Storm et al. 2003; Krapf et al. 2006) fabrication techniques make it highly necessary to establish a general theoretical approach for the analysis of the associated electrokinetic phenomena such as electroosmotic flow. For a narrow channel, since the thickness of electrical double layer (EDL) can be comparable with its radius, EDL overlapping might occur, yielding several interesting phenomena, such as ion enrichment (Pu et al. 2004) and concentration polarization (Kim et al. 2007; Nischang et al. 2006). As pointed out by Schoch et al. (2006), due to EDL overlapping, the behavior of the electroosmotic flow in a nanochannel deviates appreciably from that in a microchannel.

Both the direction and the magnitude of the electroosmotic flow in a narrow channel can affect strongly the associated applications; both of them depend upon its charged conditions, the strength of the applied electrical field and the physicochemical properties of the liquid phase. In practice, many narrow channels have ionizable functional groups and, therefore, are charged when in contact with liquid such as water. For example, pure silica channels have silanol groups (Nawrocki 1997; Liu and Maciel 1996), and titanium oxide (Hirst et al. 2005) channels bring hydroxide groups. When immersed in an aqueous environment, these functional groups dissociate or absorb ions, yielding a channel charged. In these cases, because the charged conditions depend upon the solution

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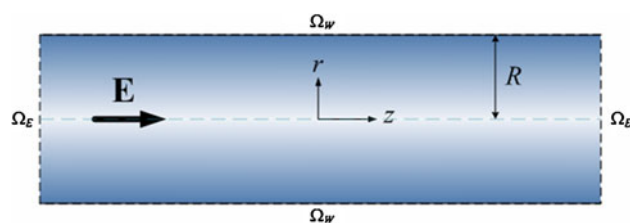
properties such as its pH and the background electrolyte concentration, they are referred to as charge-regulated surface (Hu and Bard 1997; Yeh et al. 2012a, b). This nature, however, is often neglected in relevant studies, for simplicity, and a charged surface is usually assumed to maintain at either a constant electrical potential (Ai et al. 2010; Pennathur and Santiago 2005) or constant charge density (Qiao and Aluru 2004; Wang et al. 2007; White and Bund 2008). Note that these two idealized conditions are the limiting cases of a charge-regulated surface.

The solution pH is usually adjusted by introducing reagents such as HCl and NaOH for various purposes. Due to the presence of background salts and/or buffer, this implies that besides the ionic species coming from those salts, the presence of other ionic species can be significant. For example, if solution pH deviates appreciably from 7, the presence of  $H^+$  or  $OH^-$  might be significant. In addition, the solution pH is often an important factor to the charged conditions of a charge-regulated surface. For simplicity, previous studies in electrokinetic phenomena almost always assumed that the ionic species in the liquid phase come mainly from the background salt, and only two kinds of ionic species are taken into account (Yuan et al. 2007; van der Heyden et al. 2005; Wang et al. 2010).

The above discussions suggest that extending previous analyses on electrokinetic flow to the case where the charged conditions on the channel wall depend upon solution conditions taking account of the presence of multiple ionic species is highly desirable. This is done in the present work by considering a fused silica channel of radius ranging from 50 to 500 nm containing an aqueous NaCl (background salt) solution with its pH adjusted by HCl and NaOH as an example. Because the length scale of solvent molecules is much smaller than that of the channel, a continuum model (Qu and Li 2000; Daiguji et al. 2004a, b) is applied, instead of a model based on molecular scale (Thompson 2003; Cao et al. 2010). The channel surface can assume an arbitrary level of electrical potential, which is desirable in practice. In addition to verifying the applicability of the model proposed by the available experimental data in the literature, a thorough numerical simulation is conducted to examine the influences of solution pH, background salt concentration, density of ionizable functional groups on the channel surface, and the channel radius on the volumetric flow rate and velocity distribution. The results gathered provide a useful guideline for experimentalists both to explain their data and to design electrokinetic devices.

## 2 Theory

As shown in Fig. 1, we consider the electrokinetic flow along the axis of a cylindrical nanochannel of radius



**Fig. 1** Electrokinetic flow along the axis of a cylindrical nanochannel of radius  $R$  subject to an applied uniform electrical field  $\mathbf{E}$  in the  $z$  direction;  $(r, z)$  are the computation domain of the cylindrical coordinates adopted with the origin on the axis of the channel;  $\Omega_W$  and  $\Omega_E$  are the channel wall and the input and output surfaces of that domain, respectively

$R$  subject to an applied uniform electrical field  $\mathbf{E}$ . The cylindrical coordinates  $r, \theta, z$  are adopted with the origin on the axis of the channel. Because the present problem is  $\theta$  symmetric, only the  $(r, z)$  domain needs be considered. Let  $\Omega_W$  and  $\Omega_E$  be the channel wall and the input and output surfaces of the computation domain, respectively.

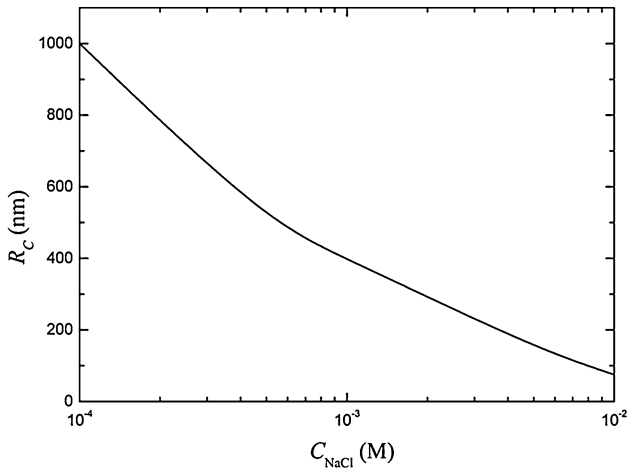
We assume that the system under consideration is at a pseudo-steady state, the liquid phase is an incompressible Newtonian fluid containing  $N$  kinds of ionic species, the flow field is in the creeping flow regime, the channel surface is nonslip and nonconducting. In addition,  $\mathbf{E}$  is relatively weak compared with the electrical field established by the channel wall, and the channel is sufficiently long so that the possible ion concentration polarization and non-uniform electric field arising from the selective transport of ions occurring at both ends of the channel is unimportant.

The channel wall is charged due to the dissociation/association of the functional group AH:  $AH \Leftrightarrow A^- + H^+$  and  $AH + H^+ \Leftrightarrow AH_2^+$ . The corresponding equilibrium constants,  $K_a$  and  $K_b$ , can be expressed as  $K_a = N_{A^-} [H^+] / N_{AH}$  and  $K_b = N_{AH_2^+} / N_{AH} [H^+]$ , with  $N_{A^-}$ ,  $N_{AH_2^+}$ ,  $N_{AH}$ , and  $[H^+]$  being the surface densities of  $A^-$ ,  $AH_2^+$ , and  $AH$  ( $\text{mol}/\text{m}^2$ ), and the molar concentration of  $H^+$ , respectively. If we let  $N_{\text{total}}$  be the total density of AH, then  $N_{\text{total}} = N_{A^-} + N_{AH} + N_{AH_2^+}$ . It can be shown that the surface charge density,  $\sigma_s$ , is

$$\sigma_s = -FN_{\text{total}} \left( \frac{K_a - K_b [H^+]_s^2}{K_b [H^+]_s^2 + [H^+]_s + K_a} \right), \quad (1)$$

where  $[H^+]_s$  and  $F$  are the value of  $[H^+]$  on  $\Omega_W$  and Faraday constant, respectively. For convenience, we define the scaled surface charge density  $\sigma_s^* = \sigma_s eR / \epsilon k_B T$ , where  $e$ ,  $\epsilon$ ,  $k_B$ , and  $T$  are the elementary charge, the permittivity of the liquid phase, Boltzmann constant, and the absolute temperature, respectively.

A perturbation approach similar to that of O'Brien and White (1978) and Ohshima (1995, 2006) is adopted to solve the present problem. The dependent variables, the



**Fig. 2** Variation of the critical radius  $R_c$  with the background salt concentration  $C_{NaCl}$  at pH 7 and  $N_{total} = 10^{-5} \text{ mol/m}^2$

electrical potential  $\phi$ , the number concentration of the  $j$ th ionic species  $n_j$ , and the fluid velocity  $\mathbf{v}$ , are all partitioned into an equilibrium component and a perturbed component. The former (latter) is the value of that variable when  $\mathbf{E}$  is absent (present). We assume that the channel is sufficiently long so that the end effect is negligible. Then, it can be shown that the present problem can be described by the following scaled equations and boundary conditions:

$$\nabla^{*2} \phi_e = \frac{(kR)^2}{\sum_{j=1}^N \alpha_{21}} \sum_{j=1}^N \alpha_{11} \exp(-\alpha_{10} \phi_e^*) \quad (2)$$

$$\nabla^{*2} \delta \phi^* = 0 \quad (3)$$

$$\eta \nabla^{*2} \mathbf{v}^* + \nabla^{*2} \phi_e^* \nabla^* \delta \phi^* = \mathbf{0} \quad (4)$$

$$\nabla^* \cdot \mathbf{v}^* = 0 \quad (5)$$

$$n_j^* = \exp(-\alpha_{10} \phi_e^*), \quad j = 1, 2, \dots, N \quad (6)$$

$$\mathbf{n} \cdot \nabla^* \phi_e^* = -\sigma_s^* \text{ on } \Omega_W \quad (7)$$

$$\mathbf{n} \cdot \nabla^* \delta \phi^* = 0 \text{ on } \Omega_W \quad (8)$$

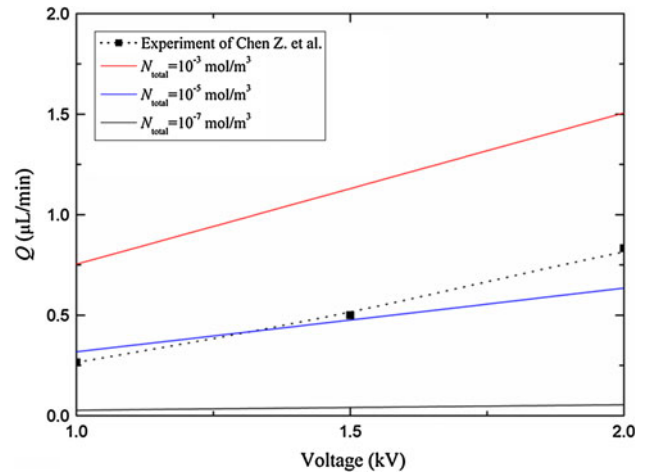
$$\mathbf{n} \cdot \nabla^* \phi_e^* = 0 \text{ on } \Omega_E \quad (9)$$

$$\mathbf{n} \cdot \nabla^* \delta \phi^* = -E_z^* \text{ on } \Omega_E \quad (10)$$

$$\mathbf{v}^* = \mathbf{0} \text{ on } \Omega_W \quad (11)$$

$$\mathbf{n} \cdot \nabla^* \mathbf{v}^* = 0 \text{ on } \Omega_E \quad (12)$$

Here, the subscript e and the prefix  $\delta$  denote the equilibrium and the perturbed properties, respectively.  $\mathbf{n}$  is the unit normal vector pointing into the system.  $\nabla^* = R\nabla$  and  $\nabla^{*2} = R^2\nabla^2$  are the scaled gradient operator and the scaled Laplace operator, respectively;  $\kappa = \left[ \sum_{j=1}^N n_{j0} (ez_j)^2 / \epsilon k_B T \right]^{1/2}$  is the reciprocal Debye screening length;  $z_j$  is the valence of ionic species  $j, j = 1, 2, \dots, N; n_j^* = n_j/n_{j0}$  with  $n_{j0}$  being the bulk



**Fig. 3** Variations of the volumetric flow rate  $Q$  with applied voltage for various values of  $N_{total}$  at  $R = 50 \mu\text{m}$ ,  $C_{NaCl} = 4.5 \times 10^{-3} \text{ M}$ , and pH 7. Curves, rescaled result from  $R = 500 \text{ nm}$ ; dashed curve with square symbol, experiment data of Chen et al. (2005)

ionic concentration of ionic species  $j$ ;  $\eta$  is the fluid viscosity;  $\mathbf{v}^* = \mathbf{v}/U^0$  with  $U^0 = \epsilon \zeta_a^2 / R \eta$  being a reference velocity.  $E_z^* = E_z / (\zeta_a / R)$ ,  $\phi_e^* = \phi_e / \zeta_a$  and  $\delta \phi^* = \delta \phi / \zeta_a$ , where  $\zeta_a (= k_B T / z_1 e)$  is the thermal potential with  $z_1$  being a reference ionic species. The parameter  $\alpha_{\beta\gamma} = z_j^\beta n_{j0}^\gamma / z_1^\beta n_{10}^\gamma$  denotes the relative concentration of ionic species  $j$  relative to  $[\text{H}^+]$ . As suggested by Eq. 4, no pressure gradient is applied. Because  $\mathbf{E}$  is weak relative to the electric field established by the channel, concentration polarization is unimportant,  $\delta n_j^* = 0$ , so is  $\nabla^{*2} \delta \phi^* = 0$  in Eq. 8, and the ionic concentration follows Boltzmann distribution in Eq. 6.

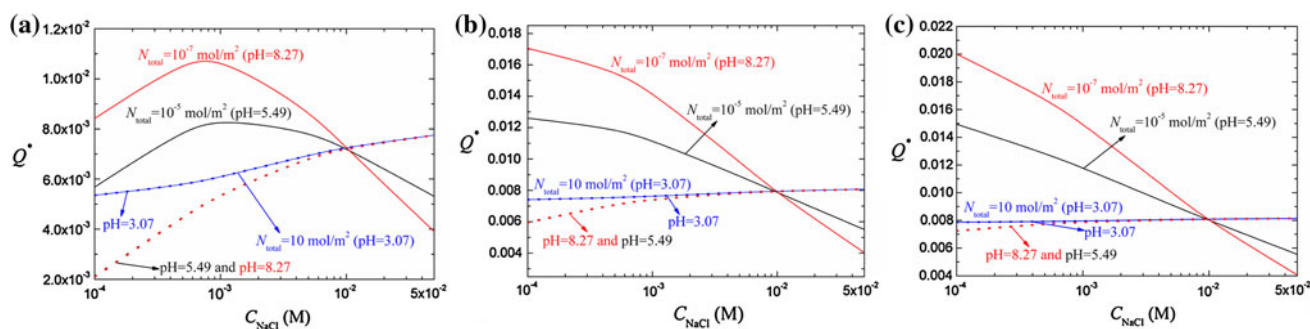
Once the velocity profile is known, the scaled volumetric flow rate,  $Q^* = Q / (\epsilon \zeta_a^2 R / \eta)$ , with  $Q$  being the volumetric flow rate can be evaluated by

$$Q^* = \iint_{S^*} (\mathbf{n} \cdot \mathbf{v}^*) dS^* \text{ on } \Omega_E, \quad (13)$$

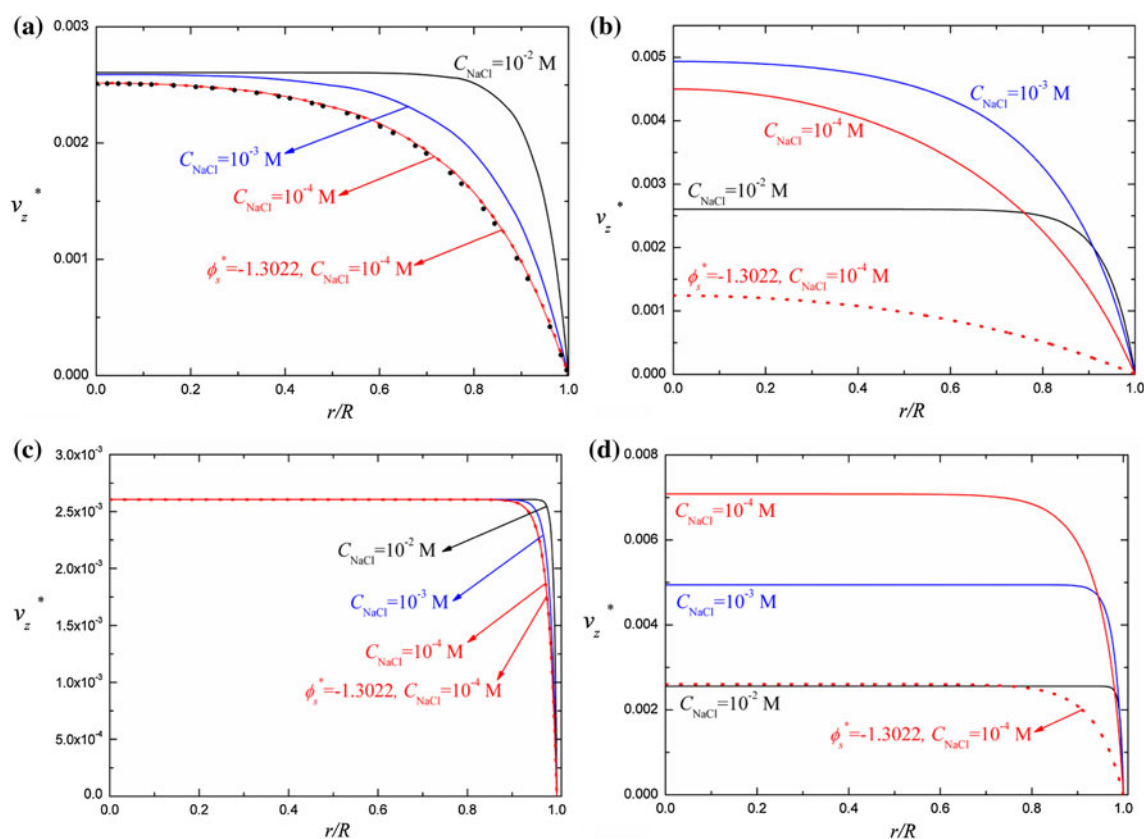
where  $S^* = S/R^2$  is the scaled cross-sectional area of the channel.

### 3 Results and discussion

The present boundary-value problem is solved numerically by FlexPDE (version 2.22; PDE Solutions, Spokane Valley, WA, 2000), which was found to be sufficiently efficient and accurate for similar problems (Hsu et al. 2004a, b). Typically, using a total of ca. 15,384 and 12,948 nodes is sufficient for the resolution of the electric and the flow fields, respectively. An error limit of  $10^{-5}$  is specified for both the electric potential and the flow velocity. For illustration, we assume that the background salt is NaCl,



**Fig. 4** Variations of the scaled volumetric flow rate  $Q^*$  with background salt concentration  $C_{NaCl}$  at various combinations of  $N_{total}$  and pH at  $R = 50 \text{ nm}$  (a),  $R = 200 \text{ nm}$  (b),  $R = 500 \text{ nm}$  (c). Solid curves, charge-regulated channel; dotted curves,  $\phi_s^* = -1.3022$



**Fig. 5** Radial distribution of  $v_z^*$  for various values of  $C_{NaCl}$  in Fig. 4a at  $N_{total} = 10 \text{ mol/m}^2$  (a),  $N_{total} = 10^{-7} \text{ mol/m}^2$  (b),  $N_{total} = 10 \text{ mol/m}^2$  in Fig. 4c (c),  $N_{total} = 10^{-7} \text{ mol/m}^2$  (d). Red dotted curves,

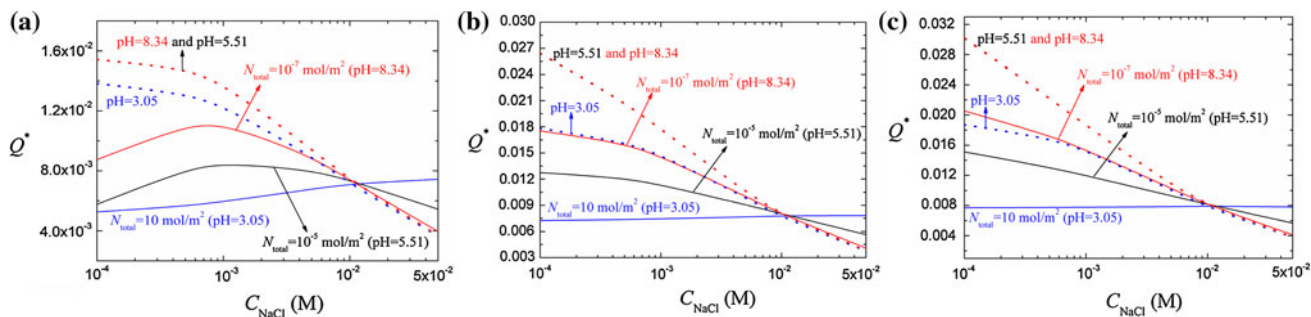
$\phi_s^* = -1.3022$  and  $C_{NaCl} = 10^{-4} \text{ M}$ ; black dotted curves, analytical solution for  $\phi_s^* = -1.3022$  and  $C_{NaCl} = 10^{-4} \text{ M}$

and the solution pH is adjusted by HCl and NaOH, so that four kinds of ionic species need be considered:  $\text{Na}^+$ ,  $\text{Cl}^-$ ,  $\text{H}^+$ , and  $\text{OH}^-$ . The concentrations of these ionic species should satisfy that for  $\text{pH} < \text{p}K_w/2$ ,  $[\text{H}^+]_0 = 10^{-\text{pH}}$ ,  $[\text{Na}^+]_0 = C_{NaCl}$ ,  $[\text{Cl}^-]_0 = C_{NaCl} + 10^{-\text{pH}} - 10^{-(\text{p}K_w - \text{pH})}$ , and  $[\text{OH}^-]_0 = 10^{-(\text{p}K_w - \text{pH})}$ , and for  $\text{pH} > \text{p}K_w/2$ ,  $[\text{H}^+]_0 = 10^{-\text{pH}}$ ,  $[\text{Na}^+]_0 = C_{NaCl} + 10^{-(\text{p}K_w - \text{pH})} - 10^{-\text{pH}}$ ,  $[\text{Cl}^-]_0 = C_{NaCl}$ , and  $[\text{OH}^-]_0 = 10^{-(\text{p}K_w - \text{pH})}$ .

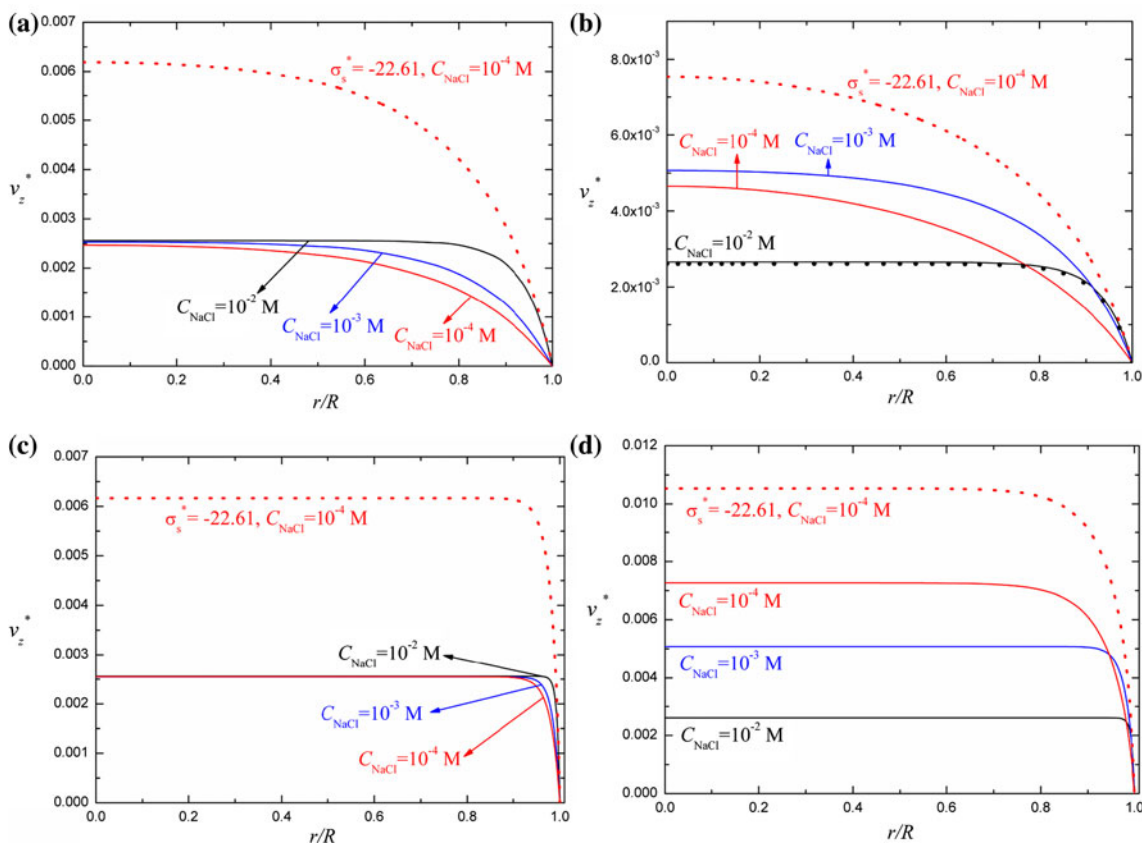
### 3.1 Influence of channel scale

To distinguish the flow in a nano-scaled channel and that in a larger-scaled one, we define a critical radius  $R_c$ , where  $Q^* \propto (S^*)^n$  for  $R_c < R$  with  $n = 1 \pm 0.02$ .  $(R - R_c)$  is a measure for the part of a channel in which the volumetric flow rate is linearly proportional to its cross-sectional area. As seen in Fig. 2,  $R_c$  decreases with increasing background NaCl





**Fig. 6** Variations of  $Q^*$  with  $C_{NaCl}$  at various combinations of  $N_{total}$ , pH, and  $R$ . **a**  $R = 50$  nm, **b**  $R = 200$  nm, **c**  $R = 500$  nm. *Solid curves*, charge-regulated surface; *dotted curves*,  $\sigma_s^* = -22.61$



**Fig. 7** Distributions of the scaled velocity  $v_z^*$  for various values of  $C_{NaCl}$  in Fig. 6a at  $N_{total} = 10 \text{ mol/m}^2$  (**a**),  $N_{total} = 10^{-7} \text{ mol/m}^2$  (**b**), that in Fig. 6c at  $N_{total} = 10 \text{ mol/m}^2$  (**c**),  $N_{total} = 10^{-7} \text{ mol/m}^2$  (**d**). *Red dotted curves*:  $\sigma_s^* = -22.61$  and  $C_{NaCl} = 10^{-4} \text{ M}$ ; *black dotted*

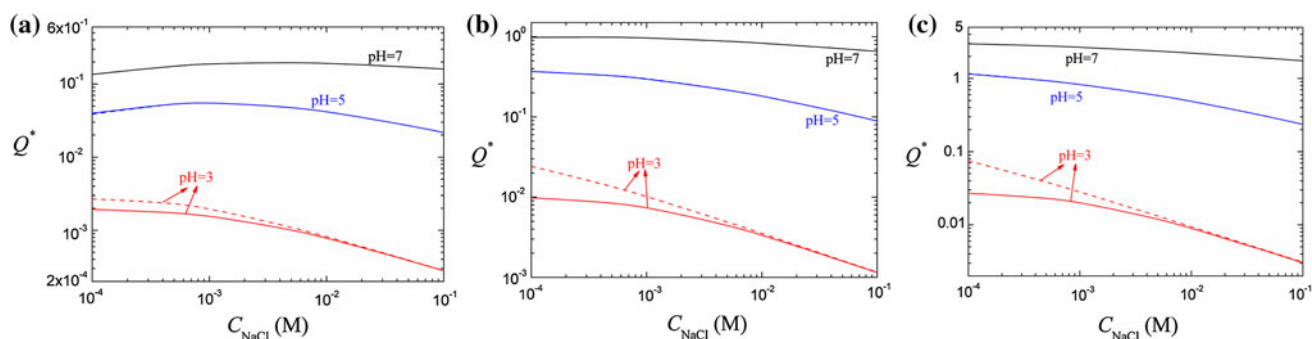
*curves in b*: analytical solution for  $\sigma_s^* = -22.61$  and  $C_{NaCl} = 10^{-2} \text{ M}$  (Chu and Ng 2012)

concentration,  $C_{NaCl}$ , in general. This is because the higher the  $C_{NaCl}$  the thinner the EDL. If  $C_{NaCl}$  is high, EDL is much thinner than channel radius so that the volumetric flow rate is proportional to its cross-sectional area. On the other hand, if  $C_{NaCl}$  is low, the EDL thickness can be comparable to the channel radius, yielding a large  $R_c$ . Note that the slope of the curve in Fig. 2 changes appreciably at  $C_{NaCl} \cong 8 \times 10^{-4} \text{ M}$ , suggesting that it is the critical level under the conditions assumed. We conclude that the flow behavior in a nano-scaled

channel is more complicated than that in a larger-scaled one, where the flow rate is essentially proportional to its cross-sectional area (Chen et al. 2005).

### 3.2 Model verification by experimental data

The applicability of the present model is examined by fitting it to the experimental data of Chen et al. (2005), where an EDTA electrolyte solution of bulk conductance



**Fig. 8** Variations of  $Q^*$  with  $C_{\text{NaCl}}$  at various combinations of pH and  $R$  at  $N_{\text{total}} = 10^{-5} \text{ mol/m}^2$ ; **a**  $R = 50 \text{ nm}$ , **b**  $R = 200 \text{ nm}$ , **c**  $R = 500 \text{ nm}$ . *Solid curves*, four kinds of ions are considered; *dashed curves*, only two kinds of ions are considered

$5 \times 10^{-4} \text{ S/cm}$  was used and the channel surface has silanol functional groups. To simulate their conditions, we assume  $\text{p}K_a = 7$ ,  $\text{p}K_b = 2$ , and  $C_{\text{NaCl}} = 4.5 \times 10^{-3} \text{ M}$ . In this case, because  $R_c$  is smaller than  $200 \text{ nm}$ ,  $Q$  can be rescaled by  $Q(R = 500 \text{ nm})$ ; that is,  $Q(R = 500 \text{ nm}) = Q(R = 200 \text{ nm}) \times (500^2/200^2)$ .

Figure 3 illustrates the variations of the volumetric flow rate  $Q$  ( $\mu\text{L/min}$ ) with applied electrical potential at various values of  $N_{\text{total}}$ . Here,  $Q$  is seen to increase linearly with the applied electrical potential, and the larger the  $N_{\text{total}}$  the larger the  $Q$ . According to the experimental data,  $N_{\text{total}} \cong 10^{-5} \text{ mol/m}^2$ , which is typical to a fused silica surface (Kirby and Hasselbrink 2004; Dolnik 2004).

### 3.3 Effect of the charged conditions

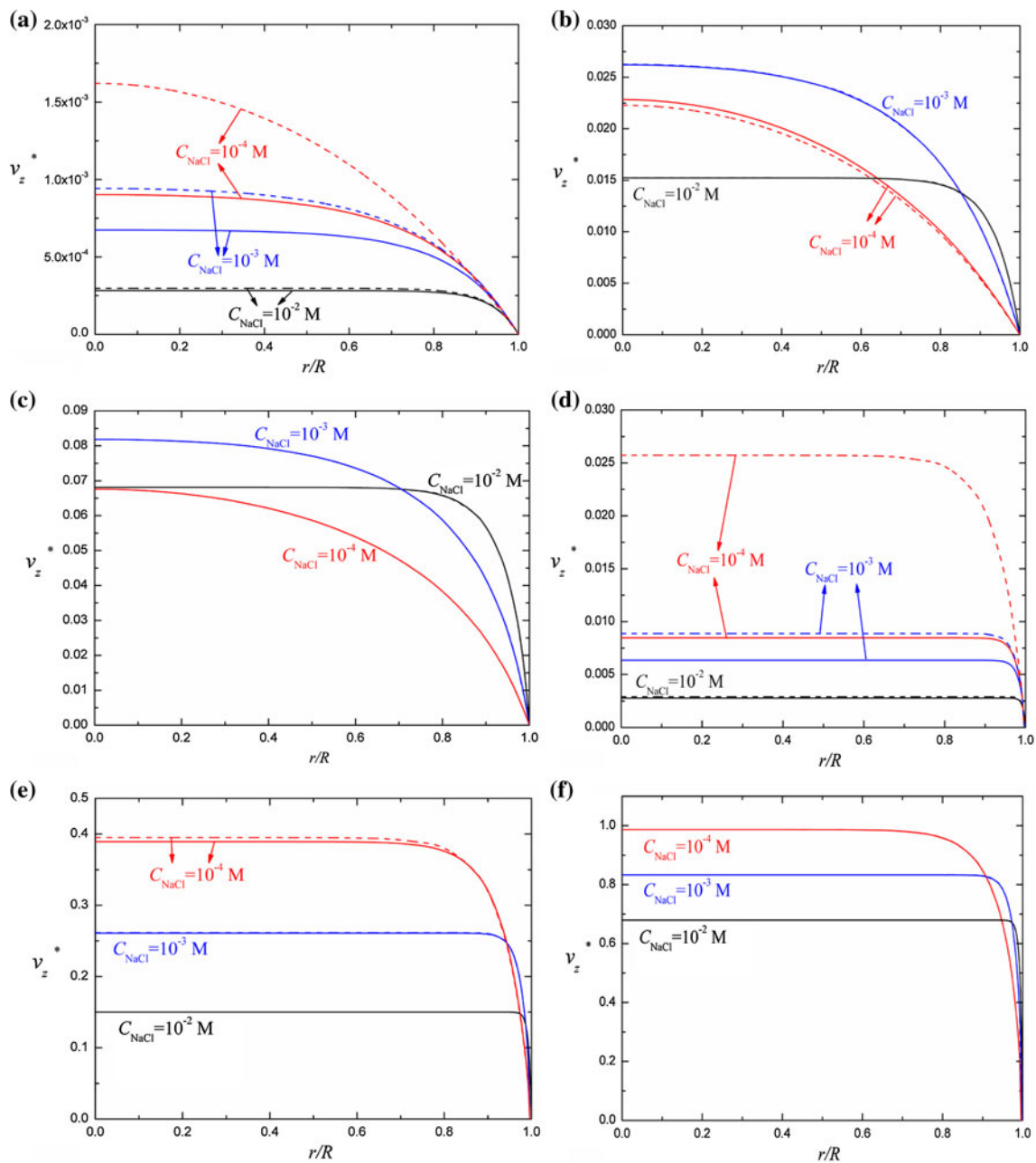
Let us examine first the effect of the charged conditions on the channel surface. Three cases are considered: a charge-regulated channel, a channel of constant charge density, and a constant electrical potential channel. It is known that the latter two models are the limiting cases of the first one. Figure 4 summarizes the variations in the scaled volumetric flow rate  $Q^*$  with  $C_{\text{NaCl}}$  for various combinations of  $N_{\text{total}}$ , pH, and  $R$ . For illustration, we assume  $E = 5 \text{ kV/m}$ . Comparison is made between the behavior of a charge-regulated surface and a constant electrical potential surface. In the latter, the scaled electrical potential on the channel surface,  $\phi_s^* = (\phi_s/\zeta_a)$  is fixed at  $-1.3022$  when  $C_{\text{NaCl}} = 10^{-2} \text{ M}$ . Note that even  $\phi_s^*$  is fixed, pH still varies with  $N_{\text{total}}$ . Therefore, the solid curves (charge-regulated) should be compared with the dotted curves (constant potential) at the same pH so that the EDL thickness is consistent.

Figure 4 shows that if  $N_{\text{total}}$  is sufficiently high ( $10 \text{ mol/m}^2$ ), the  $Q^*$  of a constant potential channel is essentially the same as that of a charge-regulated channel. However, if  $N_{\text{total}}$  is low, the behaviors of the two become different significantly. Their results have also been observed by Hsu et al. (2004a). The qualitative behavior of  $Q^*$  at  $R = 50 \text{ nm}$  (Fig. 4a) is seen to be different from that at  $R = 200$  and

$500 \text{ nm}$  (Fig. 4b, c). For example, if  $N_{\text{total}}$  is high ( $10 \text{ mol/m}^2$ ), the variation in  $Q^*$  at  $R = 50 \text{ nm}$  is much more sensitive to that at  $R = 200$  and  $500 \text{ nm}$ . This results from a rapid change in the EDL thickness/channel radius ratio. In addition, at  $R = 50 \text{ nm}$ , if  $N_{\text{total}}$  is low ( $10^{-5}$  and  $10^{-7} \text{ mol/m}^2$ ),  $Q^*$  shows a local maximum as  $C_{\text{NaCl}}$  varies, which is not seen at  $R = 200$  and  $500 \text{ nm}$ . A comparison between Fig. 5a ( $R = 50 \text{ nm}$ ) and c ( $R = 500 \text{ nm}$ ) reveals that the variation of  $v_z^*$  with  $C_{\text{NaCl}}$  in the former is more appreciable than that in the latter, which explains the behavior of  $Q^*$  seen in Fig. 4a, c. Because the behavior of  $Q^*$  as  $C_{\text{NaCl}}$  varies depends on both  $v_z^*$  and  $\phi_s^*$ , it is more complicated than that of  $v_z^*$ .

Figure 5d shows that  $v_z^*$  increases with decreasing  $C_{\text{NaCl}}$ , and  $Q^*$  decreases monotonically with  $C_{\text{NaCl}}$ ; the former results from that the surface potential increases with EDL thickness. However, as the boundary of EDL reaches the center of the channel, a further increase in its thickness might not yield a faster electrokinetic velocity. For example, as seen in Fig. 5a, c, as  $C_{\text{NaCl}}$  decreases from  $10^{-3}$  to  $10^{-4} \text{ M}$ ,  $v_z^*$  decreases accordingly because the rate of increase in  $v_z^*$  is slower than that in EDL thickness. On the other hand, if  $C_{\text{NaCl}}$  exceeds ca.  $10^{-3} \text{ M}$ , because  $\phi_s^*$  dominates,  $Q^*$  decreases with increasing  $C_{\text{NaCl}}$ , as seen in Fig. 4a. Figure 5b, d reveals that if  $N_{\text{total}}$  is low ( $10^{-7} \text{ mol/m}^2$ ), the behavior of  $v_z^*$  for a charge-regulated channel is different from that for a constant potential channel. On the other hand, if  $N_{\text{total}}$  is high ( $10 \text{ mol/m}^2$ ), the behavior of  $v_z^*$  for a charge-regulated channel is essentially the same as that for a constant potential channel even  $C_{\text{NaCl}}$  is lowered to  $10^{-4} \text{ M}$ , as seen in Fig. 5a, c. Note that the result at  $C_{\text{NaCl}} = 10^{-4} \text{ M}$  and  $\phi_s^* = -1.3022$  in Fig. 5a is close to the analytical result of Hsu et al. (2004b), which also validates the present model.

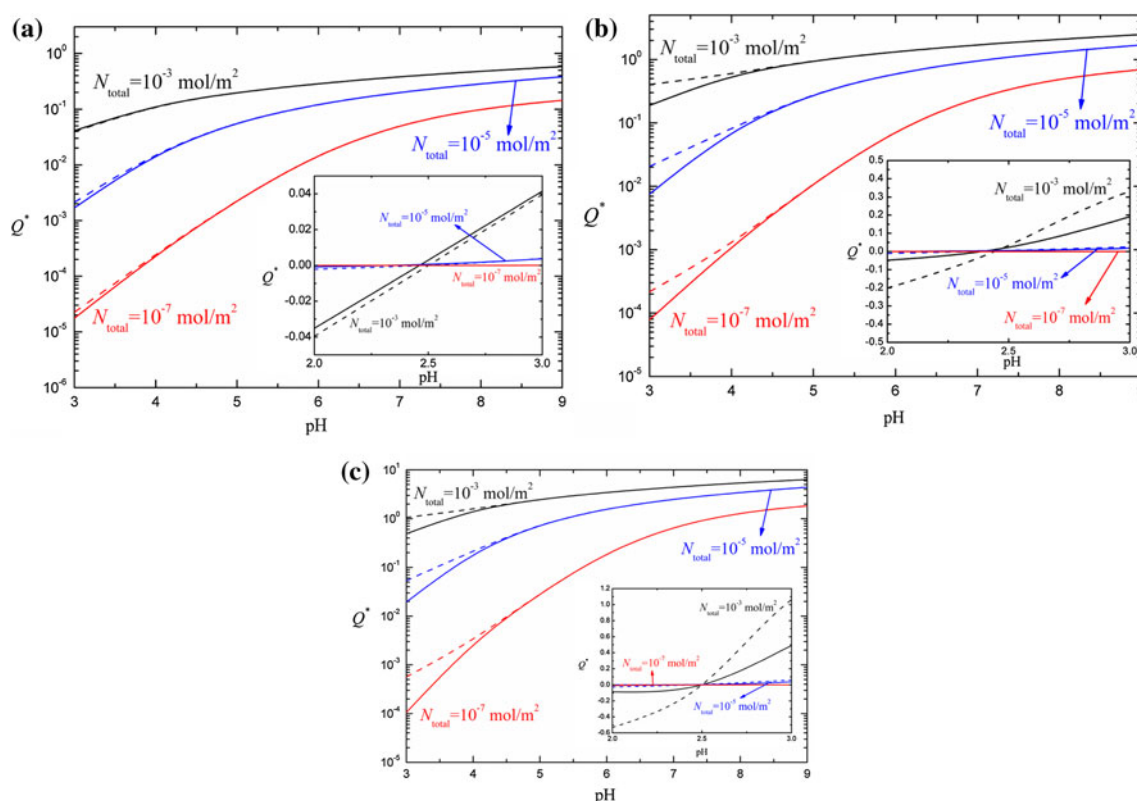
Figure 6 summarizes the variations of  $Q^*$  with  $C_{\text{NaCl}}$  at various combinations of  $N_{\text{total}}$ , pH, and  $R$ . Both the results for a charge-regulated channel and a channel with fixed charge density are presented. In the latter, the scaled charge density  $\sigma_s^*$  is fixed at  $-22.61$  (based on  $C_{\text{NaCl}} = 10^{-2} \text{ M}$ ). Note that, to achieve this, pH needs be adjusted as  $N_{\text{total}}$  varies.



**Fig. 9** Distributions of the scaled radial velocity  $v_z^*$  for various values of  $C_{\text{NaCl}}$  in Fig. 8a at pH 3 (a), pH 5 (b), pH 7 (c), that in Fig. 8c at pH 3 (d), pH 5 (e), pH 7 (f). *Solid curves*, four kinds of ions are considered; *dashed curves*, only two kinds of ions are considered

Figure 6 indicates that, in general, the lower the  $N_{\text{total}}$  and/or the higher the  $C_{\text{NaCl}}$  the closer the result of a charge-regulated channel to that of a channel of constant charge density. As seen in Fig. 6a, if  $N_{\text{total}}$  is sufficiently low (e.g.,  $10^{-7}$  mol/m<sup>2</sup>), the qualitative behavior of  $Q^*$  for the two types of channels at low  $C_{\text{NaCl}}$  is quite different: One decreases monotonically with increasing  $C_{\text{NaCl}}$ , and the other has a local maximum. This is because the rate of increase in  $\phi_s$  with decreasing  $C_{\text{NaCl}}$  for a charge-regulated channel is slower than that for a channel of constant charge

density. Note that a charge-regulated channel is of feedback nature: As its surface potential gets high,  $\text{H}^+$  is driven toward it so that the degree of dissociation of acidic functional group decreases, thereby reducing the surface potential. As mentioned previously, because the rate of increase in  $\phi_s$  as  $C_{\text{NaCl}}$  decreases is faster than that in the EDL thickness, the  $Q^*$  for the case of a channel of constant charge density increases monotonically, instead of having a local maximum as in the case of a charge-regulated channel. Figure 6 also suggests that, in general, the larger



**Fig. 10** Variations of  $Q^*$  with pH at various combinations of  $N_{\text{total}}$  and  $R$  at  $C_{\text{NaCl}} = 10^{-3}$  M; **a**  $R = 50$  nm, **b**  $R = 200$  nm, **c**  $R = 500$  nm. *Solid curves*, four kinds of ions are considered; *dashed curves*, only two kinds of ions are considered

the  $R$  the closer the results for a channel of constant charge density to those for a charge-regulated channel.

It is interesting to note that at high  $N_{\text{total}}$  ( $10 \text{ mol/m}^2$ ),  $Q^*$  increases with  $C_{\text{NaCl}}$ , which is different from the behavior of  $Q^*$  at low  $N_{\text{total}}$  and that for the case of a channel of constant charge density. As can be seen in Fig. 7a, where  $N_{\text{total}}$  is significantly high ( $10 \text{ mol/m}^2$ ), and if  $C_{\text{NaCl}}$  is low ( $10^{-4}$  M), the  $v_z^*$  for a charge-regulated channel differ significantly from that for a channel of constant charge density. Figure 7b, d shows that if  $N_{\text{total}}$  is low ( $10^{-7} \text{ mol/m}^2$ ), the  $v_z^*$  of a charge-regulated channel is similar to that of a channel of constant charge density, except that the latter overestimates  $v_z^*$ , which arises from that the rates of increase in  $\phi_s$  of the two channels as  $C_{\text{NaCl}}$  varies are different significantly. The  $v_z^*$  for the case where  $N_{\text{total}} = 10^{-7} \text{ mol/m}^2$ ,  $C_{\text{NaCl}} = 10^{-2}$  M, and  $R = 50$  in Fig. 7b is essentially the same as the corresponding analytical result (Chu and Ng 2012), which also validates the present model.

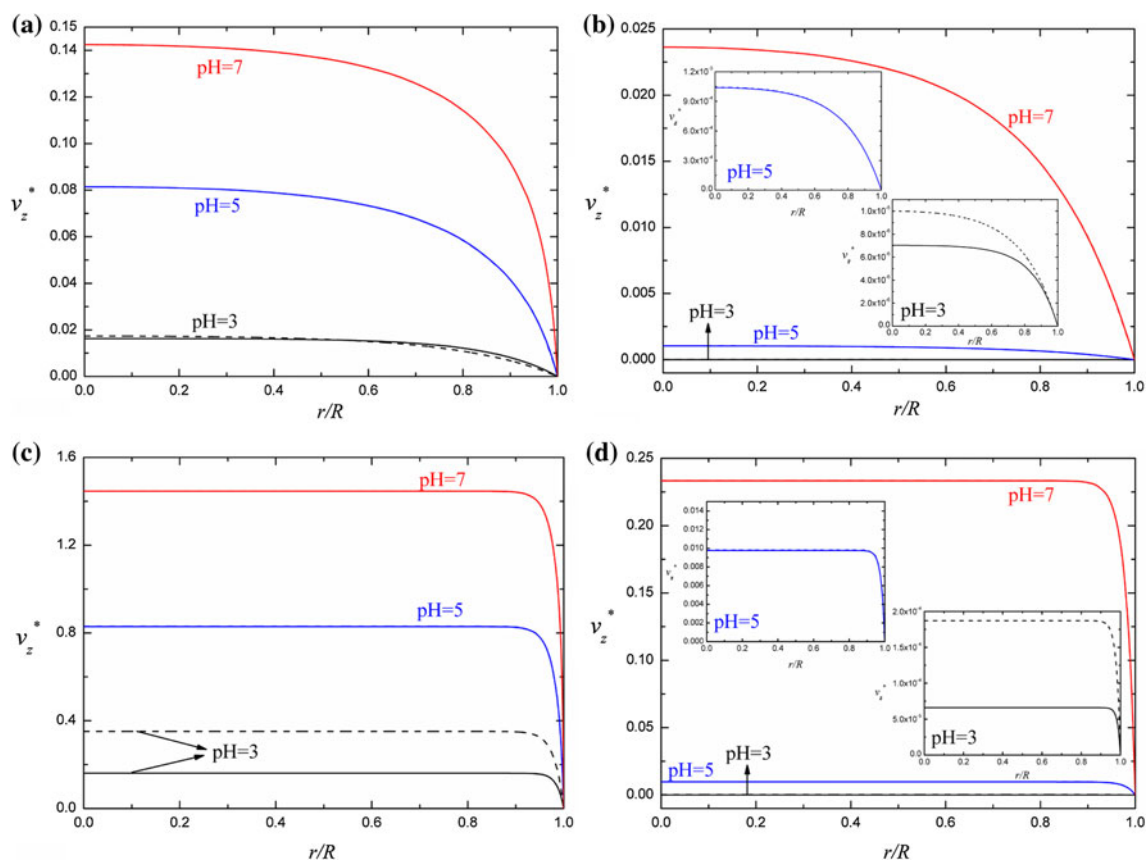
#### 3.4 Influence of pH, $N_{\text{total}}$ , and $C_{\text{NaCl}}$

Let us examine next the influences of pH,  $N_{\text{total}}$ , and  $C_{\text{NaCl}}$  on the electrokinetic behavior in a charge-regulated channel. As seen in Fig. 8, where  $E = 10$  kV/m, at a higher pH,

because the dissociation of  $\text{H}^+$  from the channel surface is more complete,  $\phi_s$  is higher and, therefore, the electrokinetic velocity is faster and  $Q^*$  is larger.

Figure 8a ( $R = 50$  nm) shows that for both pH 5 and 7,  $Q^*$  has a local maximum as  $C_{\text{NaCl}}$  varies. As mentioned previously, this results from that the EDL thickness is close to the channel radius. As can be seen in Fig. 8, if both pH and  $C_{\text{NaCl}}$  are low, assuming the presence of two types of ions only might yield an appreciable deviation in  $Q^*$ . This is because the presence of  $\text{H}^+$  is significant in this case. The types of ionic species in the liquid phase influence the EDL thickness, and therefore  $\phi_s$  and  $Q^*$ . In general,  $Q^*$  is overestimated when only two kinds of ions are considered because the EDL in this case is thicker than that in the case where the other two kinds of ions are also considered. In other words,  $\phi_s$ , and therefore,  $v_z^*$ , is overestimated when only two kinds of ions are considered. However, as seen in Fig. 9a, d, the deviation in  $v_z^*$  due to ignoring the other two kinds of ions decreases with increasing  $C_{\text{NaCl}}$ . This is expected because the higher the  $C_{\text{NaCl}}$  the more significant the presence of  $\text{Na}^+$  and  $\text{Cl}^-$ . As illustrated in Figs. 8 and 9, at pH 5 and 7, because  $\text{H}^+$  and  $\text{OH}^-$  are relatively unimportant, the  $v_z^*$  and  $Q^*$  for the case of four kinds of ions are close to those for the case of two kinds of ions. It is interesting to see in Fig. 8a (Fig. 9b) that at pH 5 and low





**Fig. 11** Distributions of the scaled radial velocity  $v_z^*$  for various values of pH for the case of Fig. 10a at  $N_{\text{total}} = 10^{-3} \text{ mol/m}^2$  (a),  $N_{\text{total}} = 10^{-7} \text{ mol/m}^2$  (b), that in Fig. 10c at  $N_{\text{total}} = 10^{-3} \text{ mol/m}^2$

(c),  $N_{\text{total}} = 10^{-7} \text{ mol/m}^2$  (d). *Solid curves* four kinds of ions are present; *dashed curves*, only two kinds of ions are present

$C_{\text{NaCl}}$ , considering only two kinds of ions will underestimate  $Q^*$  ( $v_z^*$ ). This is because that although  $\phi_s$  is overestimated when only two kinds of ions are considered, so is the EDL thickness, making  $Q^*$  ( $v_z^*$ ) underestimated, especially when EDL thickness is comparable to  $R$ .

The variations of  $Q^*$  with pH for various combinations of  $N_{\text{total}}$  and  $R$  are presented in Fig. 10, which shows that the qualitative behaviors of  $Q^*$  in all case considered are similar to each other. In general,  $Q^*$  increases with increasing pH and/or  $N_{\text{total}}$ , which results from the increase in the density of negatively charged functional groups on the channel surface.

The rate of increase in  $Q^*$  with increasing pH at lower  $N_{\text{total}}$  is faster than that at higher  $N_{\text{total}}$  because the rate of increase in the density of the charged functional group in the former is faster. This can be explained by Fig. 11a, b that although the qualitative behavior of  $v_z^*$  at  $N_{\text{total}} = 10^{-3} \text{ mol/m}^2$  is similar to that at  $N_{\text{total}} = 10^{-7} \text{ mol/m}^2$  the order of difference in  $v_z^*$  for various pH values in the latter is significantly larger than that in the former. Figure 10 reveals that neglecting the presence of  $\text{H}^+$  and  $\text{OH}^-$  can be appreciable at low pH values. In addition, consider only

two kinds of ions will overestimate  $Q^*$ , and the larger the channel the more serious the deviation. Note that the direction of electroosmotic flow is reversed for pH lower than 2.5, the point of zero charge. In this case, the channel surface becomes positively charged. This nature of a charge-regulated channel can be applied, for example, to the separation of nano-sized entities.

Figure 11 indicates that the larger the channel the more serious the deviation in  $v_z^*$  due to the consideration of two kinds of ions only. As mentioned previously, this arises from that the competition between the effect of EDL thickness and that of surface potential is more significant in small-sized channels.

## 4 Conclusions

The electrokinetic flow in a charge-regulated channel is investigated taking account of the presence of multiple ionic species so that the model considered is closer to reality than previous models. Adopting a channel with its surface bearing silanol functional groups ( $\text{p}K_a = 7$ ,  $\text{p}K_b = 2$ ) and NaCl salt

solution of molar concentration  $C_{\text{NaCl}}$  and its pH adjusted by HCl and NaOH as an example, the velocity distribution and the volumetric flow rate under various conditions are examined. The results gathered can be summarized as following. (1) The critical channel radius, the radius that the volumetric flow rate is linearly proportional to the cross-sectional area of a channel, increases with  $C_{\text{NaCl}}$ ; the plug flow assumption in a micron-scaled channel becomes invalid in a nano-scaled one. (2) As the density of the functional groups on the surface of a charge-regulated channel,  $N_{\text{total}}$ , increases (decreases), it approaches a constant potential (charge density) channel. If  $N_{\text{total}}$  is low, the behavior of a charge-regulated channel is similar to that of a channel of constant charge density at high  $C_{\text{NaCl}}$  (e.g.,  $10^{-2}$  M) and large channel radius (e.g., 200 nm). The volumetric flow rate of a small channel (e.g., 50 nm) has a local maximum as  $C_{\text{NaCl}}$  varies, which is not seen in a constant potential channel or a channel of charge density. The presence of the local maximum results from the competition between the effect of electric double layer thickness and that of channel surface potential. (3) Both the velocity and the volumetric flow rate are overestimated in most cases when only two kinds of ionic species are considered. This results from the underestimation of the electric double layer thickness at a low pH. If pH is close to 7,  $\text{Na}^+$  and  $\text{Cl}^-$  dominate, and the presence of other ionic species can be neglected. (4) The volumetric flow rate is more sensitive to the variation in pH when  $N_{\text{total}}$  is low, and the positive deviation of that quantity due to the consideration of two kinds of ions only is more serious at large channel radius. (5) The direction of electrokinetic flow can be regulated by pH, which has potential applications in, for example, separation of colloidal particles.

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