

CHARACTERISATIONS THE BIO-ACTIVE
COMPOUNDS OF BIO-OIL EXTRACTED
FROM RED MERANTI SAWDUST BY FAST
PYROLYSIS

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CHARACTERISATIONS THE BIO-ACTIVE COMPOUNDS OF BIO-OIL
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ABSTRAK

Pirolisis pantas ialah satu teknologi penukaran habakimia untuk menukar biojisim kepada produk bio-minyak. Dalam kajian ini, habuk meranti merah (RMS) dipilih sebagai biojisim suapan untuk menilai potensinya menghasilkan bio-minyak melalui pirolisis pantas. Kajian ini merangkumi objektif untuk menyiasat kesan parameter proses dalam mengoptimumkan penghasilan bio-minyak dan mencirikan bio-minyak yang diekstrak. Pirolisis cepat dijalankan dalam skala-makmal reaktor lapisan terbendalir, bersama sistem yang terdiri dari pengawal suhu, siklon, pemeluwap, gas nitrogen, meter alir and pengumpul arang dan bio-minyak. Dalam mengkaji kesan keadaan pirolisis, eksperimen dijalankan mengikut pendekatan satu-faktor-pada-satu-masa (OFAT) dengan parameter yang terlibat ialah suhu, kadar alir N_2 , masa tahanan dan saiz partikel suapan. Keputusan menunjukkan bio-oil mencapai hasil maksimum sekitar 56.3 % pada suhu 450 °C, kadar alir N_2 25 L/min dan masa tahanan 20 min. untuk saiz partikel suapan 0.3 mm. Dapat disimpulkan bahawa suhu adalah parameter yang paling berpengaruh untuk hasil bio-minyak. Pencirian fizikokimia bio-minyak menunjukkan bio-minyak tidak sesuai untuk bahan bakar pengangkutan kerana tinggi kandungan oksigen. Melalui analisis spektrometri kromatografi gas (GC-MS), fenolik adalah sebatian dominan yang dikenalpasti dalam bio-minyak. Jumlah gula dalam bio-minyak ialah 12.82 % luas termasuk hasil levoglucosan adalah 8.97 % luas. Dalam menentukan kesan rawatan basuhan biojisim, RMS dibasuh dengan air dinyahion (DI) atau asid hidroklorik (HCl) cair. Kecekapan penyingkiran AAEM dengan air DI, 1.0M HCl dan 2.0 M HCl adalah 66.39%, 93.32% dan 97.28%, masing-masing. Dari analisis FTIR, rawatan basuhan telah menguatkan ikatan kimia RMS. Untuk pengeluaran bio-minyak, bio-minyak yang diekstrak dari RMS - air DI mencapai hasil maksimum kira-kira 57.2 % pada 450 °C suhu optimum. Dalam bio-minyak yang diekstrak, RMS yang dibasuh menghasilkan lebih banyak kompaun berat dan lebih banyak levoglucosan daripada RMS mentah. Dalam kajian pyrolysis RMS yang diresapi, RMS diresapkan dengan $CaCl_2$, $CaSO_4$, $FeCl_2$ atau $FeSO_4$. Antara suapan ini, RMS - $FeSO_4$ meningkatkan proses penguraian pada suhu yang lebih rendah dengan suhu penguraian maksimum telah beralih dari 361 °C bagi RMS kawalan kepada 314 °C bagi RMS - $FeSO_4$. Melalui FTIR, resapan RMS dengan $FeSO_4$ telah melemahkan ikatan kimia dalam RMS. Dalam bio-minyak yang diekstrak, ia mengandungi sebatian berat molekul berjulat besar dan menunjukkan peningkatan dalam hasil levoglucosan. Levoglucosan adalah tertinggi dalam RMS - $FeSO_4$ iaitu 40.23 % luas, dengan hasil gula sebanyak 42.24 % luas. Dalam mengoptimumkan hasil bio-minyak, rekabentuk komposit pusat (CCD) daripada kaedah pemodelan permukaan respon (RSM) digunakan untuk membangunkan model matematik dan mengoptimumkan parameter proses. Melalui model yang diramalkan, keputusan menunjukkan keadaan proses pirolisis optimum diperolehi pada suhu 480 °C, 25 L/min kadar aliran N_2 dan 24 min masa tahanan dengan 56.5 % hasil bio-minyak dan 2.11 % ralat oleh eksperimen. Kesimpulannya, RMS mempunyai potensi untuk menghasilkan bio-minyak. Dengan rawatan lanjut ke atas bio-oil untuk menyingkirkan kandungan oksigen, bio-minyak ini boleh digunakan untuk menggantikan bahan api konvensional. Rawatan terapi RMS dengan $FeSO_4$ mendedahkan bahawa proses penguraian dapat ditingkatkan pada suhu yang lebih rendah dan meningkatkan levoglucosan dalam bio-minyak. Penemuan-penemuan ini dijangka menyediakan beberapa garis panduan dalam kajian masa depan untuk menghasilkan produk tambah nilai dari sisa lignoselulosa yang lain dan seterusnya, konsep kerajaan untuk mengalihkan sisa kepada produk-kekayaan dapat dicapai.

ABSTRACT

Fast pyrolysis is a thermochemical conversion technology to convert biomass into bio-oil product. In this study, red meranti sawdust (RMS) was selected as biomass as feedstock to evaluate its potential to produce bio-oil by fast pyrolysis. The study covers the objective to investigate the parameters effect of process in optimising the bio-oil production and characterise the extracted bio-oil. Fast pyrolysis process was conducted in a bench-scale fluidized bed reactor, with the system consist of temperature controller, cyclone, condensers, nitrogen gas, flow meter, char and bio-oil collectors. In investigating the effect of pyrolysis condition, the experiments were run according to one-factor-at-a-time (OFAT) approach with the parameters involved were temperature, N₂ flow rate, retention time and feed particles size. Results showed that bio-oil achieved maximum yield about 56.3 % at 450 °C of temperature, 25 L/min of N₂ flow rate and 20 min of retention time for 0.3 mm of feed particles size. It can be concluded that the temperature was the most influential parameter for bio-oil yield. Physicochemical characterisation of bio-oil indicated bio-oil not suitable for transportation fuel due to high oxygen content. Through gas chromatography–mass spectrometry (GC-MS) analysis, phenolic was the dominant compound identified in bio-oil. Total sugars in bio-oil was 12.82 % area including levoglucosan yield was 8.97 % area. In determining the effect of washing treatment, RMS was washed with deionised (DI) water or diluted hydrochloric (HCl) acid. The efficiency of AAEM removal by DI water, 1.0M HCl and 2.0 M HCl were 66.39 %, 93.32 %, and 97.28 %, respectively. From FTIR analysis, washing treatment had strengthened the RMS chemical bonds. For bio-oil production, bio-oil extracted from RMS - DI water achieved maximum yield about 57.2 % at 450 °C of optimum temperature. In extracted bio-oil, washed RMS produced higher heavier compound and higher levoglucosan than raw RMS. In pyrolysis of impregnated RMS study, RMS was impregnated with CaCl₂, CaSO₄, FeCl₂ or FeSO₄. Among these feedstocks, RMS - FeSO₄ enhanced the degradation process at lower temperatures with the maximum degradation of temperature has been shifted from 361 °C for RMS control to 314 °C for RMS - FeSO₄. Through FTIR analysis, impregnated RMS with FeSO₄ has weakened the RMS chemical bond. In extracted bio-oil, it consisted large range of molecular weight compounds and showed an increasing in levoglucosan yield. Levoglucosan was the highest in RMS - FeSO₄ about 40.23 % area, with 42.24 % area of total anhydrosugars yield. In optimising bio-oil yield, central composite design (CCD) of response surface methodology (RSM) modelling was employed to develop mathematical model and optimise the process parameters. Through predicted model, results showed that the optimal pyrolysis process condition was obtained at 480 °C of temperature, 25 L/min of N₂ flow rate and 24 min of retention time with 56.5 % of bio-oil yield and 2.11 % of error by experiment. Conclusion, RMS has a potential to produce bio-oil. With further treatment on bio-oil to remove oxygen content, this bio-oil can be applied to substitute conventional fuel. Impregnated treatment of RMS with FeSO₄ reveals degradation process can be enhanced at lower temperature and increases levoglucosan in bio-oil. These findings are expected to provide some guidelines in future study to produce value-added product from other lignocellulose waste and further, the government concept of divert waste to wealth-product can be achieved.

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LIST OF SYMBOLS

°C	degree Celsius
°C/s	degree Celsius per Second
cSt	centistokes
g/mol	gram/mol
kJ/kg	Kilojoule/kilogram
L/min	Litre per minute
m ³	cubic meter
min	minute
mL	millilitre
mm	millimetre
MJ/kg	Megajoule/kilogram
Mtoe	Million tons of oil equivalent
rpm	Rotation per Minute
wt. %	percentage by weight
W/mK	Watts per meter Kelvin
µm	micrometre
Y _b	bio-oil yield

LIST OF ABBREVIATIONS

AAEM	Alkali and Alkaline Earth Metal
ASEAN	Association of Southeast Asian Nations
ASTM	American Society for Testing and Materials
BC	Bio-oil Collector
C	Carbon
Ca	Calcium
CaCl ₂	Calcium Chloride
CaSO ₄	Calcium Sulphate
CC	Char Collector
CCD	Central Composite Design
CO	Carbon Monoxide
CO ₂	Carbon Dioxide
DI	Deionised
DTG	Differential Thermogravimetric
ENSYN	Renewable Fuels and Chemical from Non-Food Biomass
FeCl ₂	Iron (II) Chloride
FeSO ₄	Iron (II) Sulphate
FTeK	Fakulti Teknologi Kejuruteraan
FTIR	Fourier Transform Infrared Spectroscopy
GC-MS	Gas Chromatography – Mass Spectrometry
H ⁺	Hydrogen Ion
H ₂	Hydrogen Gas
H ₂ O	Water
HAA	Hydroxyacetaldehyde
HCl	Hydrochloride Acid
HHV	Higher Heating Value
ICP-OES	Inductively Coupled Plasma – Optical Emission Spectroscopy
K	Potassium
LHV	Lower heating value
Mg	Magnesium
N ₂	Nitrogen Gas
Na	Sodium
NCG	Non-Condensable Gases
NO _x	Nitric Oxide and Nitrogen Dioxide

NREL	National Renewable Energy Laboratory
O	Oxygen
OFAT	One Factor at a Time
PAH	Polycyclic Aromatic Hydrocarbon
pH	Potential of Hydrogen
RMS	Red Meranti Sawdust
RSM	Response Surface Methodology
TGA	Thermogravimetric Analysis
UMP	Universiti Malaysia Pahang
Zn	Zink

REFERENCES

- Abdullah, N., & Gerhauser, H. (2008). Bio-oil derived from empty fruit bunches. *Fuel*, 87, 2606–2613. <https://doi.org/10.1016/j.fuel.2008.02.011>
- Abnisa, F., Wan Daud, W.M., & Sahu, J. (2011). Optimization and characterization studies on bio-oil production from palm shell by pyrolysis using response surface methodology. *Biomass and Bioenergy*, 35(8), 3604–3616. <https://doi.org/10.1016/j.biombioe.2011.05.011>
- Açıkalmın, K., Karaca, F., & Bolat, E. (2012). Pyrolysis of pistachio shell: Effects of pyrolysis conditions and analysis of products. *Fuel*, 95, 169–177. <https://doi.org/10.1016/j.fuel.2011.09.037>
- Adam, J., Blazso, M., Meszaros, E., Stocker, M., Nilsen, M.H., Bouzga, A., Hustad, J.E., Gronli, M., & Oye, G. (2005). Pyrolysis of biomass in the presence of Al-MCM-41 type catalysts. *Fuel*, 84, 1494–1502. <https://doi.org/10.1016/j.fuel.2005.02.006>
- Agblevor, F.A., Besler, S., & Wiselogel, A.E. (1995). Fast Pyrolysis of Stored Biomass Feedstocks. *Energy & Fuels*, 9(3), 635–640. <https://doi.org/10.1021/ef00052a010>
- Akhtar, J., & NorAishah, S.A. (2012). A review on operating parameters for optimum liquid oil yield in biomass pyrolysis. *Renewable and Sustainable Energy Reviews*, 16(7), 5101–5109. <https://doi.org/10.1016/j.rser.2012.05.033>
- Azeez, A.M., Meier, D., Odermatt, J., & Willner, T. (2010). Fast pyrolysis of African and European lignocellulosic biomasses using Py-GC/MS and fluidized bed reactor. *Energy and Fuels*, 24(3), 2078–2085. <https://doi.org/10.1021/ef9012856>
- Balat, M., Balat, M., Kirtay, E., & Balat, H. (2009). Main routes for the thermo-conversion of biomass into fuels and chemicals. Part 1: Pyrolysis systems. *Energy Conversion and Management*, 50(12), 3147–3157. <https://doi.org/10.1016/j.enconman.2009.08.014>
- Ballesteros, I., Ballesteros, M., Cara, C., Saez, F., Castro, E., Manzanares, P., Negro, M.J., & Oliva, J.M. (2011). Effect of water extraction on sugars recovery from steam exploded olive tree pruning. *Bioresour. Technol.*, 102(11), 6611–6616. <https://doi.org/10.1016/j.biortech.2011.03.077>
- Beis, S.H., Onay, O., & Kockar, O.M. (2002). Fixed-bed pyrolysis of safflower seed: influence of pyrolysis parameters on product yields and compositions. *Renewable Energy*, 26, 21–32.

- Biewer, M.C. (2011). Structure Determination. Retrieved September 5, 2017, from <http://www.utdallas.edu/~biewerm/9H-analytical.pdf>
- Biomass Fuel Analysis For Energy Crop (Closed-Loop) and Wood Derived Fuel/Yardwaste (Open-Loop). (2015). Retrieved April 9, 2015, from <http://www.treepower.org/fuels/analysis.html>
- Blanco López, M.C., Blanco, C.G., Martínez-Alonso, A., & Tascón, J.M.D. (2002). Composition of gases released during olive stones pyrolysis. *Journal of Analytical and Applied Pyrolysis*, 65(2), 313–322. [https://doi.org/10.1016/S0165-2370\(02\)00008-6](https://doi.org/10.1016/S0165-2370(02)00008-6)
- Boroson, M.L., Howard, J.B., Longwell, J. P., & Peters, W.A. (1989). Product yields and kinetics from the vapor phase cracking of wood pyrolysis tars. *AIChE Journal*, 35(1), 120–128. <https://doi.org/10.1002/aic.690350113>
- Boucher, M.E., Chaala, A., Pakdel, H. & Roy, C. (2000). Bio-oils obtained by vacuum pyrolysis of softwood bark as a liquid fuel for gas turbines. Part II: Stability and ageing of bio-oil and its blends with methanol and a pyrolytic aqueous phase. *Biomass and Bioenergy*, 19(5), 351–361. [https://doi.org/10.1016/S0961-9534\(00\)00044-1](https://doi.org/10.1016/S0961-9534(00)00044-1)
- Box, G.E.P., & Wilson, K.B. (1951). On the Experimental Attainment of Optimum Conditions. *Journal of the Royal Statistical Society. Series B (Methodological)*, 13(1), 1–45.
- Bridgwater, A.V., & Bridge, S.A. (1991). A Review of Biomass Pyrolysis and Pyrolysis Technologies. In *Biomass Pyrolysis Liquids. Upgrading and Utilisation* (pp. 11–92). https://doi.org/10.1007/978-94-011-3844-4_2
- Bridgwater, A.V., & Peacocke, G.V.C. (1994). Engineering Developments in Fast Pyrolysis for Bio-oil. In *Proceeding Biomass Pyrolysis Oil Properties and Combustion Meeting, NREL* (pp. 110–127).
- Bridgwater, A.V., Meier, D., & Radlein, D. (1999). An overview of fast pyrolysis of biomass. *Organic Geochemistry*, 30(12), 1479–1493. [https://doi.org/10.1016/S0146-6380\(99\)00120-5](https://doi.org/10.1016/S0146-6380(99)00120-5)
- Bridgwater, A.V. (1999). Principles and practice of biomass fast pyrolysis processes for liquids. *Journal of Analytical and Applied Pyrolysis*, 51(1), 3–22. [https://doi.org/10.1016/S0165-2370\(99\)00005-4](https://doi.org/10.1016/S0165-2370(99)00005-4)

- Bridgwater, A.V., & Peacocke, G.V.C. (2000). Fast pyrolysis processes for biomass. *Renewable and Sustainable Energy Reviews*, 4, 1–73.
- Bridgwater, A.V. (2012). Review of fast pyrolysis of biomass and product upgrading. *Biomass and Bioenergy*, 38, 68–94. <https://doi.org/10.1016/j.biombioe.2011.01.048>
- Buckley, T. J. (1991). Calculation of higher heating values of biomass materials and waste components from elemental analyses. *Resources, Conservation and Recycling*, 5(4), 329–341.
- Butler, E., Devlin, G., Meier, D., & McDonnell, K. (2011). A review of recent laboratory research and commercial developments in fast pyrolysis and upgrading. *Renewable and Sustainable Energy Reviews*, 15(8), 4171–4186. <https://doi.org/10.1016/j.rser.2011.07.035>
- Chaalal, A., Ba, T., Garcia-Perez, M., & Roy, C. (2004). Colloidal properties of bio-oils obtained by vacuum pyrolysis of softwood bark: Aging and thermal stability. *Energy and Fuels*, 18(5), 1535–1542. <https://doi.org/10.1021/ef030156v>
- Chaiwat, W., Hasegawa, I., Kori, J., & Mae, K. (2008). Examination of degree of cross-linking for cellulose precursors pretreated with acid/hot water at low temperature. *Industrial and Engineering Chemistry Research*, 47(16), 5948–5956. <https://doi.org/10.1021/ie800080u>
- Chang, S.W., & Shaw, J.F. (2009). Biocatalysis for the production of carbohydrate esters. *New Biotechnology*, 26(3–4), 109–116. <https://doi.org/10.1016/j.nbt.2009.07.003>
- Chiaramonti, D., Oasmaa, A., & Solantausta, Y. (2007). Power generation using fast pyrolysis liquids from biomass. *Renewable and Sustainable Energy Reviews*, 11(6), 1056–1086. <https://doi.org/10.1016/j.rser.2005.07.008>
- Choi, H.S., Choi, Y.S., & Park, H.C. (2012). Fast pyrolysis characteristics of lignocellulosic biomass with varying reaction conditions. *Renewable Energy*, 42, 131–135. <https://doi.org/10.1016/j.renene.2011.08.049>
- Cindy, P.C.F., & David, J.L. (1993). Potential Applications and Markets for Biomass-Derived Levoglucosan. In *Advances in Thermochemical Biomass Conversion* (pp. 1484–1494).
- Clark, J.H. (2007). Green chemistry for the second generation biorefinery—sustainable chemical manufacturing based on biomass. *JOURNAL OF CHEMICAL TECHNOLOGY & BIOTECHNOLOGY*, 82(7), 603–609.

- Collard, F.X., Blin, J., Bensakhria, A., & Valette, J. (2012). Influence of impregnated metal on the pyrolysis conversion of biomass constituents. *Journal of Analytical and Applied Pyrolysis*, 95, 213–226. <https://doi.org/10.1016/j.jaap.2012.02.009>
- Collard, F.X., & Blin, J. (2014). A review on pyrolysis of biomass constituents: Mechanisms and composition of the products obtained from the conversion of cellulose, hemicelluloses and lignin. *Renewable and Sustainable Energy Reviews*, 38, 594–608. <https://doi.org/10.1016/j.rser.2014.06.013>
- Cornerstone Analytical Libraries. (2017). Retrieved November 24, 2017, from <http://www.cornerstoneanalytical.com/infrared-spectroscopy/>
- Coulson, M. (2006). Pyrolysis of Perennial Grasses from Southern Europe. *Pyne Newsletter*, 6–7.
- Czernik, S., & Bridgwater, A.V. (2004). Overview of applications of biomass fast pyrolysis oil. *Energy and Fuels*, 18(2), 590–598. <https://doi.org/10.1021/ef034067u>
- Demirbaş, A. (2000). Mechanisms of liquefaction and pyrolysis reactions of biomass. *Energy Conversion and Management*, 41(6), 633–646. [https://doi.org/10.1016/S0196-8904\(99\)00130-2](https://doi.org/10.1016/S0196-8904(99)00130-2)
- Demirbas, A., & Arin, G. (2002). An Overview of Biomass Pyrolysis. *Energy Sources*, 24(5), 471–482. <https://doi.org/10.1080/00908310252889979>
- Demirbas, A. (2004). Effect of initial moisture content on the yields of oily products from pyrolysis of biomass. *Journal of Analytical and Applied Pyrolysis*, 71(2), 803–815. <https://doi.org/10.1016/j.jaap.2003.10.008>
- Demirbaş, A. (2005). Relationship between Initial Moisture Content and the Liquid Yield from Pyrolysis of Sawdust. *Energy Sources*, 27(9), 823–830. <https://doi.org/10.1080/00908310490479042>
- Di Blasi, C. (2002). Modeling intra- and extra-particle processes of wood fast pyrolysis. *AIChE Journal*, 48(10), 2386–2397.
- Di Blasi, C., Carmen, B., & Antonio, G. (2007). Effects of Diammonium Phosphate on the Yields and Composition of Products from Wood Pyrolysis. *Industrial & Engineering Chemistry Research*, 46(2), 430–438.

- Di Blasi, C., Branca, C., & Galgano, A. (2008). Thermal and catalytic decomposition of wood impregnated with sulfur- and phosphorus-containing ammonium salts. *Polymer Degradation and Stability*, 93(2), 335–346. <https://doi.org/10.1016/j.polymdegradstab.2007.12.003>
- Dickerson, T., & Soria, J. (2013). Catalytic Fast Pyrolysis: A Review. *Energies*, 6(1), 514–538. <https://doi.org/10.3390/en6010514>
- Diebold, J.P., & Bridgwater, A.V. (1997). Overview of Fast Pyrolysis of Biomass for the Production of Liquid Fuels. In *Developments in Thermochemical Biomass Conversion* (pp. 5–23). Springer Netherlands. https://doi.org/10.1007/978-94-009-1559-6_1
- Eibner, S., Broust, F., Blin, J., & Julbe, A. (2015). Catalytic effect of metal nitrate salts during pyrolysis of impregnated biomass. *Journal of Analytical and Applied Pyrolysis*, 113, 143–152. <https://doi.org/10.1016/j.jaap.2014.11.024>
- Ellens, C.J., & Brown, R.C. (2012). Optimization of a free-fall reactor for the production of fast pyrolysis bio-oil. *Bioresource Technology*, 103(1), 374–380. <https://doi.org/10.1016/j.biortech.2011.09.087>
- Eom, I.Y., Kim, K.H., Kim, J.Y., Lee, S.M., Yeo, H.M., Choi, I.G., & Choi, J.W. (2011). Characterization of primary thermal degradation features of lignocellulosic biomass after removal of inorganic metals by diverse solvents. *Bioresource Technology*, 102(3), 3437–3444. <https://doi.org/10.1016/j.biortech.2010.10.056>
- Eom, I-Y., Kim, J-Y., Kim, T-S., Lee, S-M., Choi, D., Choi, I-G., & Choi, J.-W. (2012). Effect of essential inorganic metals on primary thermal degradation of lignocellulosic biomass. *Bioresource Technology*, 104, 687–694. <https://doi.org/10.1016/j.biortech.2011.10.035>
- Eric Meier. (2015). *WOOD! Identifying and Using Hundreds of Woods Worldwide*. The Wood Database.
- Fahmi, R., Bridgwater, A.V., Darvell, L.I., Jones, J. M., Yates, N., Thain, S., & Donnison, I. S. (2007). The effect of alkali metals on combustion and pyrolysis of Lolium and Festuca grasses, switchgrass and willow. *Fuel*, 86(10–11), 1560–1569. <https://doi.org/10.1016/j.fuel.2006.11.030>
- Fahmi, R., Bridgwater, A.V., Donnison, I., Yates, N., & Jones, J.M. (2008). The effect of lignin and inorganic species in biomass on pyrolysis oil yields, quality and stability. *Fuel*, 87(7), 1230–1240. <https://doi.org/10.1016/j.fuel.2007.07.026>

- Fisher, T., Hajaligol, M., Waymack, B., & Kellogg, D. (2002). Pyrolysis behavior and kinetics of biomass derived materials. *Journal of Analytical and Applied Pyrolysis*, 62(2), 331–349. [https://doi.org/10.1016/S0165-2370\(01\)00129-2](https://doi.org/10.1016/S0165-2370(01)00129-2)
- Fratini, E., Bonini, M., Oasmaa, A., Solantausta, Y., Teiseira, J., & Baglioni, P. (2006). SANS analysis of the microstructural evolution during the ageing of pyrolysis oils from biomass. *American Chemical Society*, 22, 306–312.
- Gani, A., & Naruse, I. (2007). Effect of cellulose and lignin content on pyrolysis and combustion characteristics for several types of biomass. *Renewable Energy*, 32(4), 649–661. <https://doi.org/10.1016/j.renene.2006.02.017>
- García-Pérez, M., Chaala, A., & Roy, C. (2002). Vacuum pyrolysis of sugarcane bagasse. *Journal of Analytical and Applied Pyrolysis*, 65(2), 111–136. [https://doi.org/10.1016/S0165-2370\(01\)00184-X](https://doi.org/10.1016/S0165-2370(01)00184-X)
- García-Pérez, M., Chaala, A., Pakdel, H., Kretschmer, D., & Roy, C. (2007). Characterization of bio-oils in chemical families. *Biomass and Bioenergy*, 31(4), 222–242. Retrieved from <http://www.sciencedirect.com/science/article/pii/S0961953406001838>
- García-Pérez, M., Adams, T.T., Goodrum, J.W., Geller, D.P., & Das, K. C. (2007). Production and Fuel Properties of Pine Chip Bio-oil / Biodiesel Blends. *Energy*, (10), 2363–2372.
- García-Pérez, M., Wang, X.S., Shen, J., Rhodes, M.J., Tian, F., Lee, W., Wu, H., & Li, C. (2008). Fast Pyrolysis of Oil Mallee Woody Biomass: Effect of Temperature on the Yield and Quality of Pyrolysis Products. *Industrial & Engineering Chemistry Research*, 47(6), 1846–1854. <https://doi.org/10.1021/ie071497p>
- Ghafoori, S. (2013). *Modeling, Simulation and Optimization of Advanced Oxidation Processes for Treatment of Polymeric*. Thesis of Doctor of Philosophy, Program of Chemical Engineering, Toronto, Ontario, Canada.
- Goh, C.S., Tan, K.T., Lee, K.T., & Bhatia, S. (2010). Bio-ethanol from lignocellulose: Status, perspectives and challenges in Malaysia. *Bioresource Technology*, 101(13), 4834–4841. <https://doi.org/10.1016/j.biortech.2009.08.080>
- Gupta, A.K., & Lilley, D.G. (2003). Thermal Destruction of Wastes and Plastics. In *Plastics and Environment* (pp. 629–696). Wiley-Interscience.

- Hamelinck, C.N., Van Hooijdonk, G., & Faaij, A.P.C. (2005). Ethanol from lignocellulosic biomass: Techno-economic performance in short-, middle- and long-term. *Biomass and Bioenergy*, 28(4), 384–410. <https://doi.org/10.1016/j.biombioe.2004.09.002>
- Harinen, S. (2004). *Analysis of the top phase fraction of wood pyrolysis liquids*. University of Jyväskylä.
- Heidari, A., Stahl, R., Younesi, H., Rashidi, A., Troeger, N., & Ghoreyshi, A.A. (2014). Effect of process conditions on product yield and composition of fast pyrolysis of *Eucalyptus grandis* in fluidized bed reactor. *Journal of Industrial and Engineering Chemistry*, 20(4), 2594–2602. <https://doi.org/10.1016/j.jiec.2013.10.046>
- Heo, H.S., Park, H.J., Yim, J., Sohn, J. M., Park, J., Kim, S., Ryu, C., Jeon, J., & Park, Y. (2010). Influence of operation variables on fast pyrolysis of *Miscanthus sinensis* var. *purpurascens*. *Bioresource Technology*, 101(10), 3672–3677. <https://doi.org/10.1016/j.biortech.2009.12.078>
- Heo, H.S., Park, H.J., Park, Y., Ryu, C., Suh, D.J., Suh, Y., Yim, J., & Kim, S. (2010). Bio-oil production from fast pyrolysis of waste furniture sawdust in a fluidized bed. *Bioresource Technology*, 101 Suppl(1), S91-6. <https://doi.org/10.1016/j.biortech.2009.06.003>
- Hu, S., Jiang, L., Wang, Y., Su, S., Sun, L., Xu, B., He, L., & Xiang, J. (2015). Effects of inherent alkali and alkaline earth metallic species on biomass pyrolysis at different temperatures. *Bioresource Technology*, 192, 23–30. <https://doi.org/10.1016/j.biortech.2015.05.042>
- Ingram, L., Mohan, D., Bricka, M., Steele, P., Strobel, D., Crocker, D., Mitchell, B., Mohammad, J., Cantrell, K., & Pittman, C. U. (2008). Pyrolysis of wood and bark in an auger reactor: Physical properties and chemical analysis of the produced bio-oils. *Energy and Fuels*, 22(1), 614–625. <https://doi.org/10.1021/ef700335k>
- Isahak, W.N.R.W., Hisham, M.W.M., Yarmo, M.A., & Yun Hin, T. (2012). A review on bio-oil production from biomass by using pyrolysis method. *Renewable and Sustainable Energy Reviews*, 16(8), 5910–5923. <https://doi.org/10.1016/j.rser.2012.05.039>
- Islam, M.N., & Ani, F.N. (1998). Pyrolytic oil from fluidised bed pyrolysis of oil palm shell and its characterisation. *Renewable Energy* 06, 17, 73–84.

- Jendoubi, N., Broust, F., Commandre, J.M., Mauviel, G., Sardin, M., & Lédé, J. (2011). Inorganics distribution in bio oils and char produced by biomass fast pyrolysis: The key role of aerosols. *Journal of Analytical and Applied Pyrolysis*, 92(1), 59–67. <https://doi.org/10.1016/j.jaap.2011.04.007>
- Jiang, H., Song, L., Cheng, Z., Chen, J., Zhang, L., Zhang, M., Hu, M., Li, J., & Li, J. (2015). Influence of pyrolysis condition and transition metal salt on the product yield and characterization via Huadian oil shale pyrolysis. *Journal of Analytical and Applied Pyrolysis*, 112, 230–236. <https://doi.org/10.1016/j.jaap.2015.01.020>
- Kan, T., Strezov, & Evans, T.J. (2016). Lignocellulosic biomass pyrolysis: A review of product properties and effects of pyrolysis parameters. *Renewable and Sustainable Energy Reviews*, 57, 126–1140. <https://doi.org/10.1016/j.rser.2015.12.185>
- Kang, B.S., Lee, K.H., Park, H.J., Park, Y.K., & Kim, J.S. (2006). Fast pyrolysis of radiata pine in a bench scale plant with a fluidized bed: Influence of a char separation system and reaction conditions on the production of bio-oil. *Journal of Analytical and Applied Pyrolysis*, 76(1–2), 32–37. <https://doi.org/10.1016/j.jaap.2005.06.012>
- Kersten, S.R.A., Van Swaij, W.P.M., Lefferts, L., & Seshan, K. (2007). Chapter 6. Options for Catalysis in the Thermochemical Conversion of Biomass into Fuels. In *Catalysis for Renewables: from feedstock to Energy Production*. Wiley-VCH.
- Kim, S.W., Koo, B.S., Ryu, J.W., Lee, J.S., Kim, C.J., Lee, D.H., Kim, G.R., & Choi, S. (2013). Bio-oil from the pyrolysis of palm and Jatropha wastes in a fluidized bed. *Fuel Processing Technology*, 108, 118–124. <https://doi.org/10.1016/j.fuproc.2012.05.002>
- Kleen, M., & Gellerstedt, G. (1995). Influence of inorganic species on the formation of polysaccharide and lignin degradation products in the analytical pyrolysis of pulps. *Journal of Analytical and Applied Pyrolysis*, 35(1), 15–41. [https://doi.org/10.1016/0165-2370\(95\)00893-J](https://doi.org/10.1016/0165-2370(95)00893-J)
- Koenig, J. A. (n.d.). Amount and Concentration: Making and Diluting Solutions. Retrieved December 30, 2015, from <http://www.mathcentre.ac.uk/resources/uploaded/module2textbooklike.pdf>
- Krishna Prasad K., Sangen, E., & Visser, P. (1985). Woodburning Cookstoves. In *Advances in Heat Transfer* (pp. 159–310).
- Larson, D. (2008). Biofuel production technologies: Status, prospects and implications for trade and development. *United Nations Conference on Trade and Development*, 1–41.

- Lédé, J., Broust, F., Ndiaye, F.T., & Ferrer, M. (2007). Properties of bio-oils produced by biomass fast pyrolysis in a cyclone reactor. *Fuel*, 86(12–13), 1800–1810. <https://doi.org/10.1016/j.fuel.2006.12.024>
- Lehto, J., Oasmaa, A., Solantausta, Y., Kytö, M., & Chiaramonti, D. (2013). Fuel oil quality and combustion of fast pyrolysis bio-oils. *VTT Publications*, (87), 79. <https://doi.org/http://dx.doi.org/10.1016/j.apenergy.2013.11.040>
- Liew, W.H., Hassim, M.H., & Ng, D.K.S. (2014). Review of evolution, technology and sustainability assessments of biofuel production. *Journal of Cleaner Production*. <https://doi.org/10.1016/j.jclepro.2014.01.006>
- Lu, Q., Li, W-Z., & Zhu, X-F. (2009). Overview of fuel properties of biomass fast pyrolysis oils. *Energy Conversion and Management*, 50(5), 1376–1383. <https://doi.org/10.1016/j.enconman.2009.01.001>
- Lu, Q., Yang, X-C., Dong, C-Q., Zhang, Z-F., Zhang, X-M., & Zhu, X-F. (2011). Influence of pyrolysis temperature and time on the cellulose fast pyrolysis products: Analytical Py-GC/MS study. *Journal of Analytical and Applied Pyrolysis*, 92(2), 430–438. Retrieved from <http://www.sciencedirect.com/science/article/pii/S0165237011001495>
- Luo, Z., Wang, S., Liao, Y., Zhou, J., Gu, Y., & Cen, K. (2004). Research on biomass fast pyrolysis for liquid fuel. *Biomass and Bioenergy*, 26(5), 455–462. <https://doi.org/10.1016/j.biombioe.2003.04.001>
- Lv, D., Xu, M., Liu, X., Zhan, Z., Li, Z., & Yao, H. (2010). Effect of cellulose, lignin, alkali and alkaline earth metallic species on biomass pyrolysis and gasification. *Fuel Processing Technology*, 91(8), 903–909. <https://doi.org/10.1016/j.fuproc.2009.09.014>
- Malaysia Energy Centre. (2002). Retrieved June 24, 2015, from www.ptm.org.my
- Mamleeva, V., Bourbigot, S., Le Bras, M., & Yvon, J. (2009). The facts and hypotheses relating to the phenomenological model of cellulose pyrolysis: Interdependence of the steps. *J. Anal. Appl. Pyrolysis*, 84(1), 1–17.
- Mayer, Z.A., Apfelbacher, A., & Hornung, A. (2012). Effect of sample preparation on the thermal degradation of metal-added biomass. *Journal of Analytical and Applied Pyrolysis*, 94, 170–176. <https://doi.org/10.1016/j.jaap.2011.12.008>

- Mazlan, M.A.F., Uemura, Y., Osman, N.B., & Yusup, S. (2015). Fast pyrolysis of hardwood residues using a fixed bed drop-type pyrolyzer. *Energy Conversion and Management*, 98, 208–214. <https://doi.org/10.1016/j.enconman.2015.03.102>
- McGrath, T.E., Chan, W.G., & Hajaligol, M.R. (2003). Low temperature mechanism for the formation of polycyclic aromatic hydrocarbons from the pyrolysis of cellulose. *Journal of Analytical and Applied Pyrolysis*, 66(1–2), 51–70. [https://doi.org/10.1016/S0165-2370\(02\)00105-5](https://doi.org/10.1016/S0165-2370(02)00105-5)
- Meier, D. (1999). New methods for chemical and physical characterization and round robin testing. In *Fast Pyrolysis of Biomass: A Handbook*. Newbury: CPL Press.
- Meier, S. (2013). Elemental Analysis of Wood Fuels NYSERDA’s Promise to New Yorkers: NYSERDA provides resources, expertise and objective information so New Yorkers can make confident, informed energy decisions . *NYSERDA Report 13-13*, (June).
- Mekhilef, S., Saidur, R., Safari, A., & Mustaffa, W.E.S.B. (2011). Biomass energy in Malaysia: Current state and prospects. *Renewable and Sustainable Energy Reviews*, 15(7), 3360–3370. <https://doi.org/10.1016/j.rser.2011.04.016>
- Michael, L.B., Jack, B.H., John, P.L. and William, A.P. (1989). Heterogeneous cracking of wood pyrolysis tars over fresh wood char surfaces. *Energy Fuels*, 3(6), 735–740.
- Michael, H.K., John, N., Christopher, J., & Nachtsheim, W.W. (2011). *No Title* (4th editio). McGraw-Hill Education.
- Mofijur, M., Masjuki, H.H., Kalam, M.A., Hazrat, M.A., Liaquat, A.M., Shahabuddin, M., & Varman, M. (2012). Prospects of biodiesel from *Jatropha* in Malaysia. *Renewable and Sustainable Energy Reviews*, 16(7), 5007–5020. <https://doi.org/10.1016/j.rser.2012.05.010>
- Mohan, D., Pittman, C.U., & Steele, P.H. (2006). Pyrolysis of Wood/Biomass for Bio-oil: A Critical Review. *Energy & Fuels*, 20(3), 848–889. <https://doi.org/10.1021/ef0502397>
- Montgomery, D.C. (2012). *Design and Analysis of Experiments* (8th Editio). John-Wiley & Sons. Inc. Tempe, Arizona.
- Morf, P., Hasler, P., & Nussbaumer, T. (2002). Mechanisms and kinetics of homogeneous secondary reactions of tar from continuous pyrolysis of wood chips. *Fuel*, 81(7), 843–853. Retrieved from <http://www.sciencedirect.com/science/article/pii/S0016236101002162>

- Mourant, D., Wang, Z., He, M., Wang, X.S., Garcia-Perez, M., Ling, K., & Li, C-Z. (2011). Mallee wood fast pyrolysis: Effects of alkali and alkaline earth metallic species on the yield and composition of bio-oil. *Fuel*, *90*(9), 2915–2922. <https://doi.org/10.1016/j.fuel.2011.04.033>
- Mszros, E., Vrhegyi, G., Jakab, E., & Marosvlgyi, B. (2004). Thermogravimetric and Reaction Kinetic Analysis of Biomass Samples from an Energy Plantation Thermogravimetric and Reaction Kinetic Analysis of Biomass Samples from an Energy Plantation. *Review Literature And Arts Of The Americas*, (10), 497–507. <https://doi.org/10.1021/ef034030>
- Mullen, C.A., & Boateng, A.A. (2011). Characterization of water insoluble solids isolated from various biomass fast pyrolysis oils. *Journal of Analytical and Applied Pyrolysis*, *90*(2), 197–203. Retrieved from <http://www.sciencedirect.com/science/article/pii/S0165237010001798>
- Naik, S.N., Goud, V.V., Rout, P.K., & Dalai, A.K. (2010). Production of first and second generation biofuels: A comprehensive review. *Renewable and Sustainable Energy Reviews*, *14*(2), 578–597. <https://doi.org/10.1016/j.rser.2009.10.003>
- Nanda, S., Kozinski, J.A., & Dalai, A. K. (2016). Lignocellulosic biomass: A review of conversion technologies and fuel products. *Current Biochemical Engineering*, *3*(1), 24–36. <https://doi.org/10.2174/2213385203666150219232000>
- Neves, D., Thunman, H., Matos, A., Tarelho, L., & Gómez-Barea, A. (2011). Characterization and prediction of biomass pyrolysis products. *Progress in Energy and Combustion Science*, *37*(5), 611–630. <https://doi.org/10.1016/j.pecs.2011.01.001>
- Ngo, T-A., Kim, J., & Kim, S-S. (2013). Fast pyrolysis of palm kernel cake using a fluidized bed reactor: Design of experiment and characteristics of bio-oil. *Journal of Industrial and Engineering Chemistry*, *19*(1), 137–143. <https://doi.org/10.1016/j.jiec.2012.07.015>
- Nigam, P.S., & Singh, A. (2011). Production of liquid biofuels from renewable resources. *Progress in Energy and Combustion Science*, *37*(1), 52–68. <https://doi.org/10.1016/j.pecs.2010.01.003>
- Nik-Azar, M., Hajaligol, M.R., Sorahbi, M., & Dabir, B. (1996). Mineral matter effects in rapid pyrolysis of beech wood. *Fuel Processing Technology*, *3820*(96), 7–17.

- Nowakowski, D.J., Bridgwater, A.V., Elliott, D.C., Meier, D., & de Wild, P. (2010). Lignin fast pyrolysis: Results from an international collaboration. *Journal of Analytical and Applied Pyrolysis*, 88(1), 53–72. <https://doi.org/10.1016/j.jaap.2010.02.009>
- Nowakowski, D.J., Jones, J.M., Brydson, R.M.D., & Ross, A.B. (2007). Potassium catalysis in the pyrolysis behaviour of short rotation willow coppice. *Fuel*, 86(15), 2389–2402. <https://doi.org/10.1016/j.fuel.2007.01.026>
- Nurbakhsh Said. (1989). *Thermal Decomposition of Charring Materials*. Michigan State University.
- Oasmaa, A., Leppamaki, E., Koponen, P., Levander, J., & Tapola, E. (1997). Physical characterisation of biomass-based pyrolysis liquids application of standard fuel oil analyses. *VTT Publications*, (306). [https://doi.org/10.1016/S0140-6701\(98\)97220-4](https://doi.org/10.1016/S0140-6701(98)97220-4)
- Oasmaa, A., & Czernik, S. (1999). Fuel oil quality of biomass pyrolysis oil - State of the art for the end users. *Energy & Fuels*, 13(4), 914–921. <https://doi.org/10.1021/ef980272b>
- Oasmaa, A., & Peacocke, C. (2001). A guide to physical property characterisation of biomass-derived fast pyrolysis liquids. *VTT Publications*, (450), 2–65.
- Oasmaa, A., Kuoppala, E., Gust, S., & Solantausta, Y. (2003). Fast pyrolysis of forestry residue. 1. Effect of extractives on phase separation of pyrolysis liquids. *Energy and Fuels*, 17(1), 1–12. <https://doi.org/10.1021/ef020088x>
- Oasmaa, A., Kuoppala, E., & Solantausta, Y. (2003). Fast pyrolysis of forestry residue. 2. Physicochemical composition of product liquid. *Energy and Fuels*, 17(2), 433–443. <https://doi.org/10.1021/ef020206g>
- Oasmaa, A., & Kuoppala, E. (2003). Fast Pyrolysis of Forestry Residue. 3. Storage Stability of Liquid Fuel. *Energy & Fuels*, 17(4), 1075–1084.
- Oasmaa, A., Elliott, D.C., & Muller, S. (2009). Quality control in fast pyrolysis bio-oil production and use. *Environmental Progress and Sustainable Energy*, 28(3), 404–409. <https://doi.org/10.1002/ep.10382>
- Onay, O. (2007). Influence of pyrolysis temperature and heating rate on the production of bio-oil and char from safflower seed by pyrolysis, using a well-swept fixed-bed reactor. *Fuel Processing Technology*, 88(5), 523–531. <https://doi.org/10.1016/j.fuproc.2007.01.001>

- Ong, H.C., Mahlia, T.M.I., & Masjuki, H.H. (2011). A review on energy scenario and sustainable energy in Malaysia. *Renewable and Sustainable Energy Reviews*, 15(1), 639–647. <https://doi.org/10.1016/j.rser.2010.09.043>
- Ortega, J.V., Renehan, A.M., Liberatore, M.W., & Herring, A.M. (2011). Physical and chemical characteristics of aging pyrolysis oils produced from hardwood and softwood feedstocks. *Journal of Analytical and Applied Pyrolysis*, 91(1), 190–198. <https://doi.org/10.1016/j.jaap.2011.02.007>
- Ozcimen, D., & Karaosmanoglu, F. (2004). Production and characterization of bio-oil and biochar from rapeseed cake. *Renewable Energy*, 29(5), 779–787.
- Park, H.J., Dong, J-I., Jeon, J-K., Park, Y-K., Yoo, K-S., Kim, S-S., Kim, J., & Kim, S. (2008). Effects of the operating parameters on the production of bio-oil in the fast pyrolysis of Japanese larch. *Chemical Engineering Journal*, 143(1–3), 124–132. <https://doi.org/10.1016/j.cej.2007.12.031>
- Park, H.J., Park, Y-K., Dong, J-I., Kim, J-S., Jeon, J-K., Kim, S-S., Kim, J., Song, B., Park, J., & Lee, K-J. (2009). Pyrolysis characteristics of Oriental white oak: Kinetic study and fast pyrolysis in a fluidized bed with an improved reaction system. *Fuel Processing Technology*, 90(2), 186–195. <https://doi.org/10.1016/j.fuproc.2008.08.017>
- Part 1: Literature Review and Model Simulations. (2005). In *Biomass Fast Pyrolysis in a Fluidized Bed: Product Cleaning by In-situ Filtration* (pp. 8773–8785).
- Radlein, D. (2002). Study of levoglucosan production – a review biomass. In *A Handbook: Fast pyrolysis of biomass. Vol. 2*. Newbury: CPL Press.
- Ran Xu. (2010). *Development of advanced technologies for biomass pyrolysis*. (Doctoral Dissertation). The University of Western Ontario, London, Ontario.
- Rath, J., Wolfinger, M.G., & Stainer, G. (2003). Heat of Wood Pyrolysis. *Fuel*, 82(1), 81–91.
- Raveendran, K., Ganesh, A., & Khilart, K.C. (1995). Influence of mineral matter pyrolysis characteristics on biomass, 74(12), 1812–1822.
- Richards, G. N. and Zheng, G. (1991). Influence of Metal Ion and Salts on the Products from Pyrolysis of Wood: Application to Thermochemical Processing of Newspring and Biomass. *J. Anal. Appl. Pyrolysis*, 21(1–2), 133–146.

- Rowell, R.M. (1984). *The Chemistry of Solid Wood*.
- Scheirs, J., Camino, G., & Tumiatti, W. (2001). Overview of water evolution during the thermal degradation of cellulose. *European Polymer Journal*, 37(5), 933–942. [https://doi.org/10.1016/S0014-3057\(00\)00211-1](https://doi.org/10.1016/S0014-3057(00)00211-1)
- Scott, D.S., Piskorz, J. (1984). The Continuous Flash Pyrolysis of Biomass. *J. Chem. Eng*, 62(3), 404–412.
- Scott, D.S., Majerski, P., Piskorz, J., & Radlein, D. (1999). A second look at fast pyrolysis of biomass—the RTI process. *Journal of Analytical and Applied Pyrolysis*, 51(1–2), 23–37. [https://doi.org/10.1016/S0165-2370\(99\)00006-6](https://doi.org/10.1016/S0165-2370(99)00006-6)
- Scott, D.S., Paterson, L., Piskorz, J., & Radlein, D. (2000). Pretreatment of poplar wood for fast pyrolysis: Rate of cation removal. *Journal of Analytical and Applied Pyrolysis*, 57(2), 169–176. [https://doi.org/10.1016/S0165-2370\(00\)00108-X](https://doi.org/10.1016/S0165-2370(00)00108-X)
- Shafizadeh, F. (1982). Introduction to pyrolysis of biomass. *Journal of Analytical and Applied Pyrolysis*, 3(4), 283–305.
- Shafizadeh, F., Furneaux, R.H., Cochran, T.G., Scholl, J.P., & Sakai, Y. (1979). Production of levoglucosan and glucose from pyrolysis of cellulosic materials. *Journal of Applied Polymer Science*, 23(12), 3525–3539. <https://doi.org/10.1002/app.1979.070231209>
- Sharma, R.K., Wooten, J.B., Baliga, V.L., Lin, X., Geoffrey Chan, W., & Hajjaligol, M. R. (2004). Characterization of chars from pyrolysis of lignin. *Fuel*, 83(11–12), 1469–1482. <https://doi.org/10.1016/j.fuel.2003.11.015>
- Shen, J., Wang, X-S., Garcia-Perez, M., Mourant, D., Rhodes, M.J., & Li, C-Z. (2009). Effects of particle size on the fast pyrolysis of oil mallee woody biomass. *Fuel*, 88(10), 1810–1817. <https://doi.org/10.1016/j.fuel.2009.05.001>
- Shen, D.K., Gu, S., & Bridgwater, A.V. (2010). Study on the pyrolytic behaviour of xylan-based hemicellulose using TG-FTIR and Py-GC-FTIR. *Journal of Analytical and Applied Pyrolysis*, 87(2), 199–206. <https://doi.org/10.1016/j.jaap.2009.12.001>
- Shihadeh A., & H. S. (2002). Impact of Biomass Pyrolysis Oil Process Conditions on Ignition Delay in Compression Ignition Engines. *Energy & Fuels*, 16(3), 552–561.
- Sinha, S., Jhalani, A., Ravi, M. R., & Ray, A. (2000). Modelling of Pyrolysis in Wood : A Review. *Journal of Solar Energy Society of India (SESI)*, 10 (1), 41–62.

- Sudo, S., Takahashi, F., & Tekeuchi, M. (1989). *Chemical Properties of Biomass*. (A. H. C. W. Kitani, O, Ed.). New York: Gordon and Breach Science.
- The Japan Institute of Energy. (2010). Bahagian 7: Situasi biojisim di negara- negara Asia. In *The Asian Biomass Handbook: A Guide for Biomass Production and Utilization* (pp. 200–243).
- Tillman, D. A. (1991). *The Combustion of Solid Fuels and Wastes*. ACADEMIC PRESS. INC.
- Timber Wood Supply. (2017). Retrieved November 23, 2017, from <http://timberwoodsupplymalaysia.com.my/>
- Tröger, N., Richter, D., & Stahl, R. (2013). Effect of feedstock composition on product yields and energy recovery rates of fast pyrolysis products from different straw types. *Journal of Analytical and Applied Pyrolysis*, 100, 158–165. <https://doi.org/10.1016/j.jaap.2012.12.012>
- Uzun, B.B., Pütün, A.E., & Pütün, E. (2007). Composition of products obtained via fast pyrolysis of olive-oil residue: Effect of pyrolysis temperature. *Journal of Analytical and Applied Pyrolysis*, 79(1–2 SPEC. ISS.), 147–153. <https://doi.org/10.1016/j.jaap.2006.12.005>
- Vaca Garcia, C. (2008). Biomaterials. In J. C. and F. Deswarte (Ed.), *Introduction to Chemicals from Biomass*. John-Wiley and Sons, Ltd.
- Vamvuka, D. (2011). Bio-oil, solid and gaseous biofuels from biomass pyrolysis processes - An overview. *International Journal of Energy Research*, 35(10), 835–862.
- Van de Velden, M., Baeyens, J., Brems, A., Janssens, B., & Dewil, R. (2010). Fundamentals, kinetics and endothermicity of the biomass pyrolysis reaction. *Renewable Energy*, 35(1), 232–242. Retrieved from <http://www.sciencedirect.com/science/article/pii/S0960148109001803>
- Várhegyi, G., Grønli, M.G., & Di Blasi, C. (2004). Effects of Sample Origin, Extraction, and Hot-Water Washing on the Devolatilization Kinetics of Chestnut Wood. *Industrial & Engineering Chemistry Research*, 43(10), 2356–2367. <https://doi.org/10.1021/ie034168f>
- Venderbosch, R.H., & Prins, W. (2011). Fast Pyrolysis. In *Wiley Series in Renewable Resource: Thermochemical Processing of Biomass: Conversion into Fuels, Chemicals and Power*. (pp. 124–156). John Wiley and Sons, Ltd.

- Vick, C.B. (2007). Adhesive Bonding of Wood Materials. In U. S. Department of Agriculture (Ed.), *The Encyclopedia of Wood* (p. 2). Skyhorse Publishing, Inc. Delaware corporation.
- Vigouroux, R.Z. (2001). *Pyrolysis of Biomass*. Faculty of Mississippi State University.
- Wang, X., Kersten, S.R.A., Prins, W., Van Swaaij, & Wim, P.M. (2005). Biomass Pyrolysis in a Fluidized Bed Reactor. Part 2: Experimental Validation of Model Results. *Ind. Eng. Chem. Res.*, *44*(23), 8786–8795. <https://doi.org/10.1021/ie050486y>
- Wang, K., Zhang, J., Shanks, B.H., & Brown, R.C. (2015). The deleterious effect of inorganic salts on hydrocarbon yields from catalytic pyrolysis of lignocellulosic biomass and its mitigation. *Applied Energy*, *148*, 115–120. <https://doi.org/10.1016/j.apenergy.2015.03.034>
- Wang, P., Zhan, S., Yu, H., Xue, X., & Hong, N. (2010). The effects of temperature and catalysts on the pyrolysis of industrial wastes (herb residue). *Bioresource Technology*, *101*(9), 3236–3241. <https://doi.org/10.1016/j.biortech.2009.12.082>
- Water and Energy Consumer Association of Malaysia. (2009). Retrieved June 24, 2015, from www.ptm.org.my/cabd/pdf/GreenTechnologyWaterEnergySector.pdf
- Wei, L., Xu, S., Zhang, L., Zhang, H., Liu, C., Zhu, H., & Liu, S. (2006). Characteristics of fast pyrolysis of biomass in a free fall reactor. *Fuel Processing Technology*, *87*(10), 863–871. <https://doi.org/10.1016/j.fuproc.2006.06.002>
- Wildschut, J. (2009). Chapter 1: An Introduction to the Hydroprocessing of Biomass Derived Pyrolysis oil. In *Pyrolysis oil upgrading to transportation fuels by catalytic hydrotreatment*. (pp. 5–9). University of Groningen. Retrieved from <http://www.rug.nl/research/portal>
- Xiu, S., & Shahbazi, A. (2012). Bio-oil production and upgrading research: A review. *Renewable and Sustainable Energy Reviews*, *16*(7), 4406–4414. <https://doi.org/10.1016/j.rser.2012.04.028>
- Xu, J., Jiang, J., Chen, J., & Sun, Y. (2010). Biofuel production from catalytic cracking of woody oils. *Bioresource Technology*, *101*(14), 5586–5591. <https://doi.org/10.1016/j.biortech.2010.01.148>
- Yang, H., Yan, R., Chen, H., Lee, D.H., & Zheng, C. (2007). Characteristics of hemicellulose, cellulose and lignin pyrolysis. *Fuel*, *86*(12–13), 1781–1788. <https://doi.org/10.1016/j.fuel.2006.12.013>

- Zafar, S. (2011). Biomass Energy in Malaysia. Retrieved April 23, 2015, from <http://cleantechsolutions.wordpress.com/2011/07/15>
- Zafar, S. (2015). Biomass Resources in Malaysia. Retrieved June 26, 2015, from <http://www.bioenergyconsult.com/biomass-energy-malaysia/>
- Zaror, C.A., & Pyle, D.L. (1982). The pyrolysis of biomass: A general review. *Proceedings of the Indian Academy of Science (Engg. Sci.)*, 5(December), 269–285.
- Zhang, L., Liu, R., Yin, R., & Mei, Y. (2013). Upgrading of bio-oil from biomass fast pyrolysis in China: A review. *Renewable and Sustainable Energy Reviews*, 24, 66–72. <https://doi.org/10.1016/j.rser.2013.03.027>
- Zhang, J. (1996). *Pyrolysis of Biomass*. Thesis of Master Degree of Science, Chemical Engineering, Mississippi State University.
- Zhang, Q., Chang, J., Wang, T., & Xu, Y. (2007). Review of biomass pyrolysis oil properties and upgrading research. *Energy Conversion and Management*, 48(1), 87–92. <https://doi.org/10.1016/j.enconman.2006.05.010>