

Winter 2-12-2019

# Solar thermoelectricity Via Advanced Latent Heat Storage

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## Recommended Citation

Olsen, Michele L.; Toberer, Eric S.; Ginley, David S.; Parilla, Philip A.; Warren, Emily L.; Martinez, Aaron D.; Rea, Jonathan E.; Hardin, Corey Lee; Oshman, Christopher J.; and Siegel, Nathan P., "Solar thermoelectricity Via Advanced Latent Heat Storage" (2019). *Other Faculty Research and Publications*. 132.

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(12) **United States Patent**  
**Olsen et al.**

(10) **Patent No.:** **US 10,203,164 B2**  
(45) **Date of Patent:** **Feb. 12, 2019**

(54) **SOLAR THERMOELECTRICITY VIA  
ADVANCED LATENT HEAT STORAGE**

(52) **U.S. Cl.**  
CPC ..... *F28D 20/021* (2013.01); *F24J 2/07*  
(2013.01); *F24J 2/34* (2013.01); *F24J 2/4649*  
(2013.01);

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Siegel**, Lewisburg, PA (US)

(58) **Field of Classification Search**  
CPC ..... *F28D 20/021*; *F28D 20/028*; *F28D 15/06*;  
*F24J 2/07*; *F24J 2/34*; *F24J 2/4649*;  
(Continued)

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Siegel**, Lewisburg, PA (US)

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(\* ) Notice: Subject to any disclaimer, the term of this  
patent is extended or adjusted under 35  
U.S.C. 154(b) by 267 days.

(21) Appl. No.: **15/290,051**

(22) Filed: **Oct. 11, 2016**

(65) **Prior Publication Data**

US 2017/0102192 A1 Apr. 13, 2017

**Related U.S. Application Data**

(60) Provisional application No. 62/315,923, filed on Mar.  
31, 2016, provisional application No. 62/240,342,  
filed on Oct. 12, 2015.

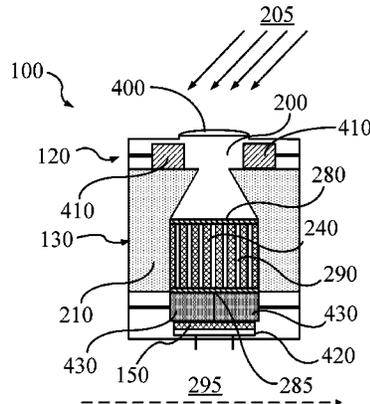
(51) **Int. Cl.**  
*F28D 20/02* (2006.01)  
*H01L 35/30* (2006.01)

(Continued)

(57) **ABSTRACT**

An aspect of the present disclosure is a system that includes  
a thermal valve having a first position and a second position,  
a heat transfer fluid, and an energy converter where, when in  
the first position, the thermal valve prevents the transfer of  
heat from the heat transfer fluid to the energy converter, and  
when in the second position, the thermal valve allows the  
transfer of heat from the heat transfer fluid to the energy  
converter, such that at least a portion of the heat transferred  
is converted to electricity by the energy converter.

**14 Claims, 19 Drawing Sheets**





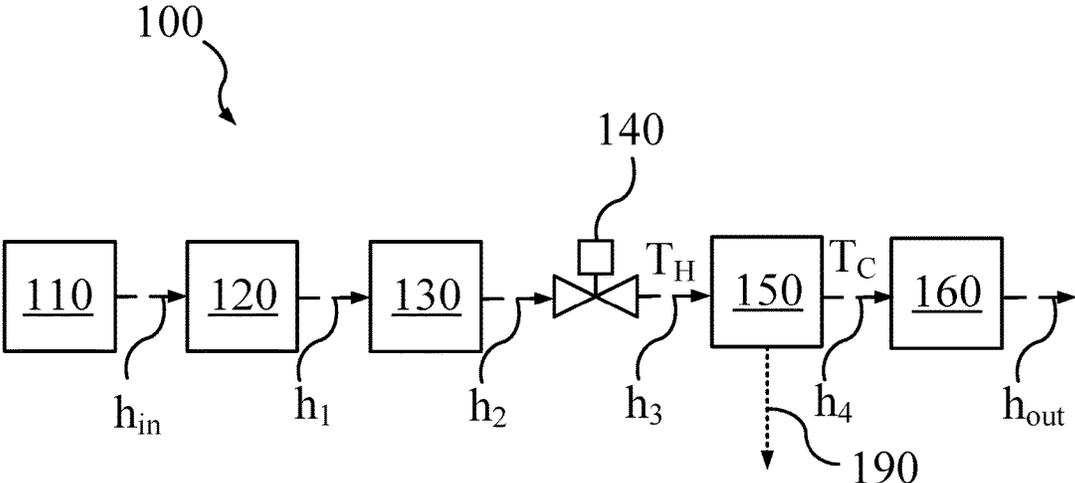


Figure 1

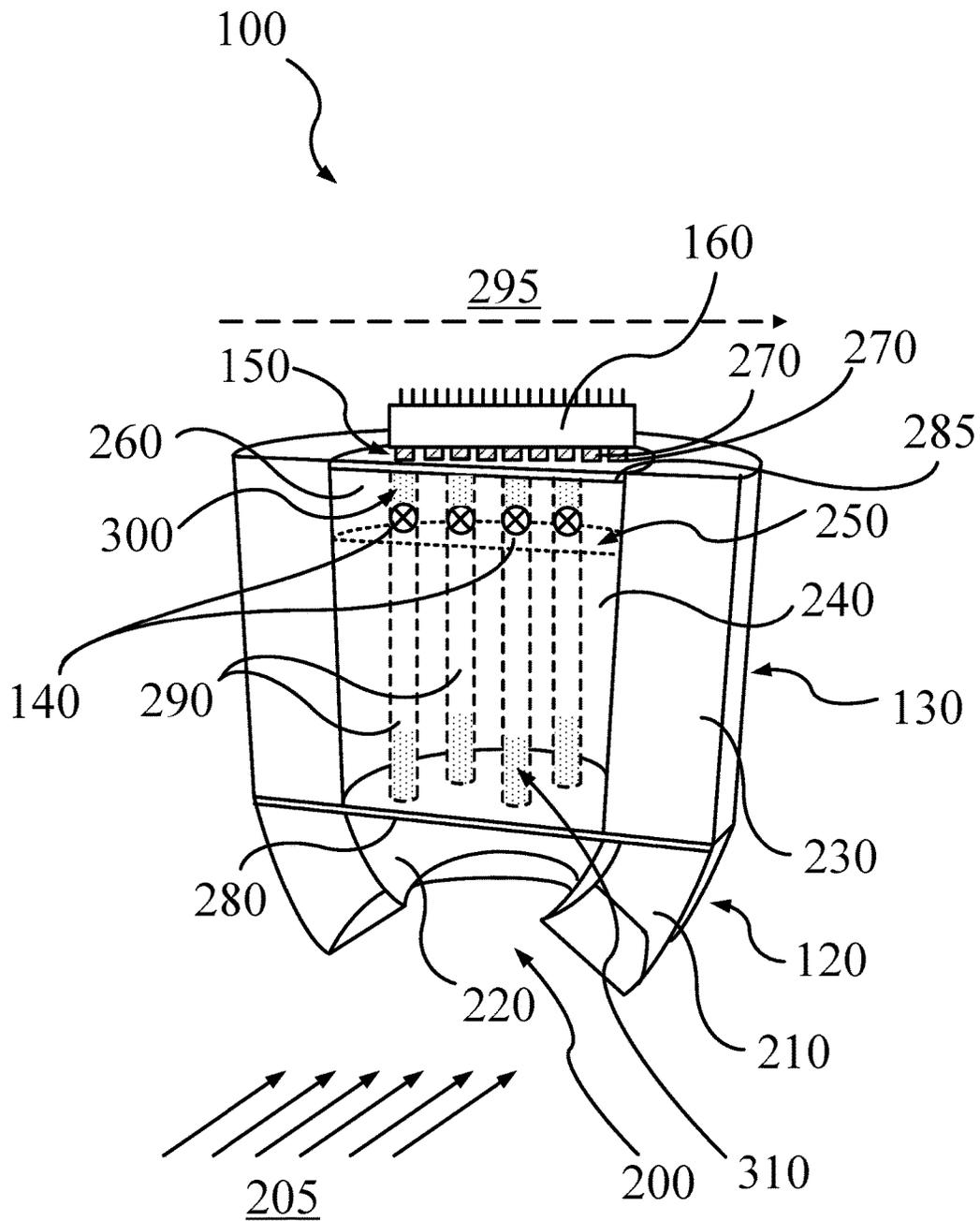


Figure 2

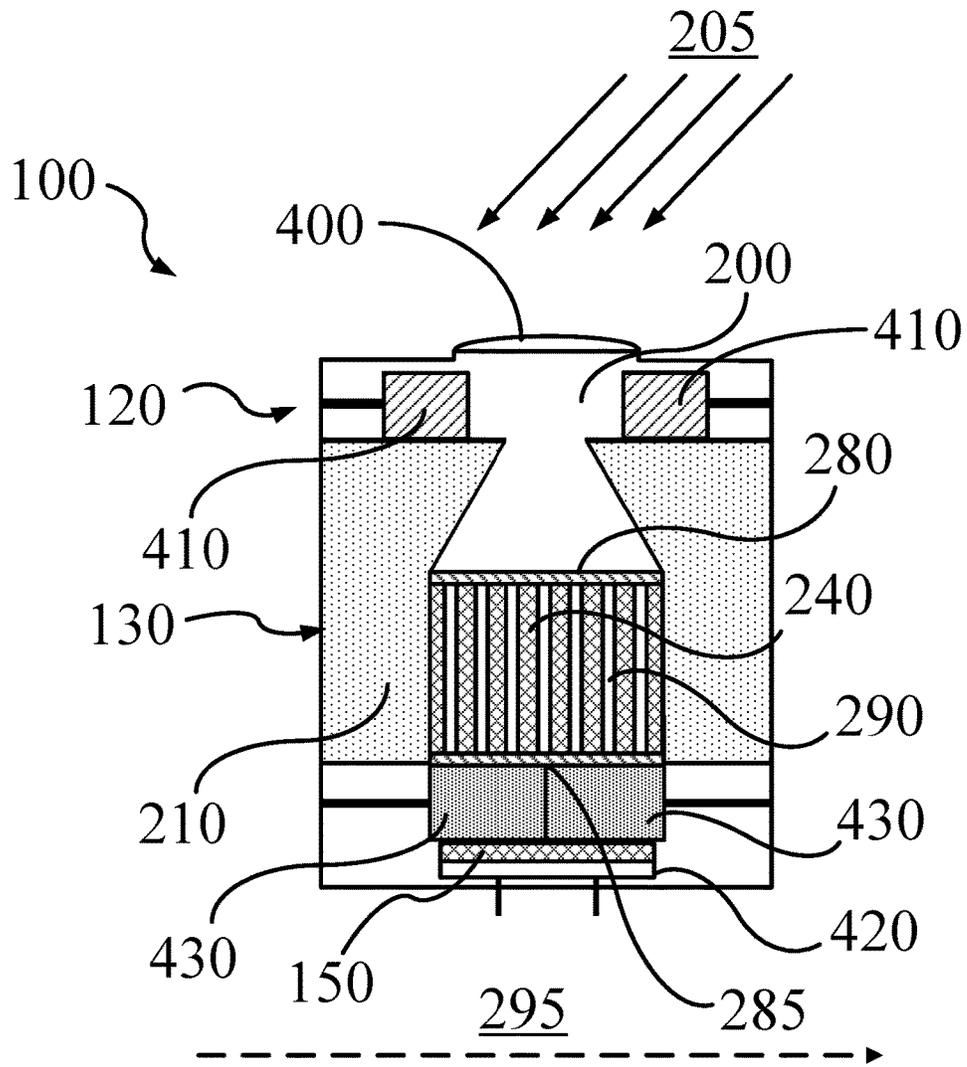


Figure 3a

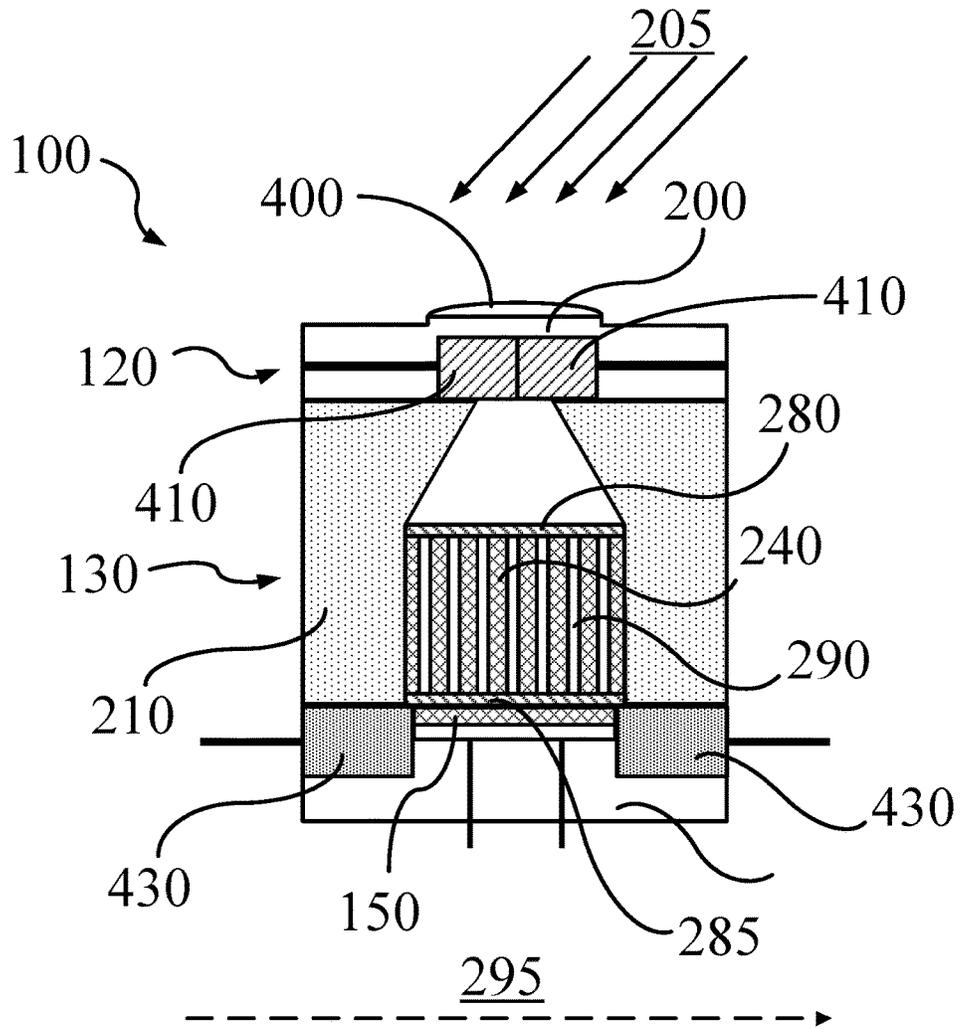


Figure 3b

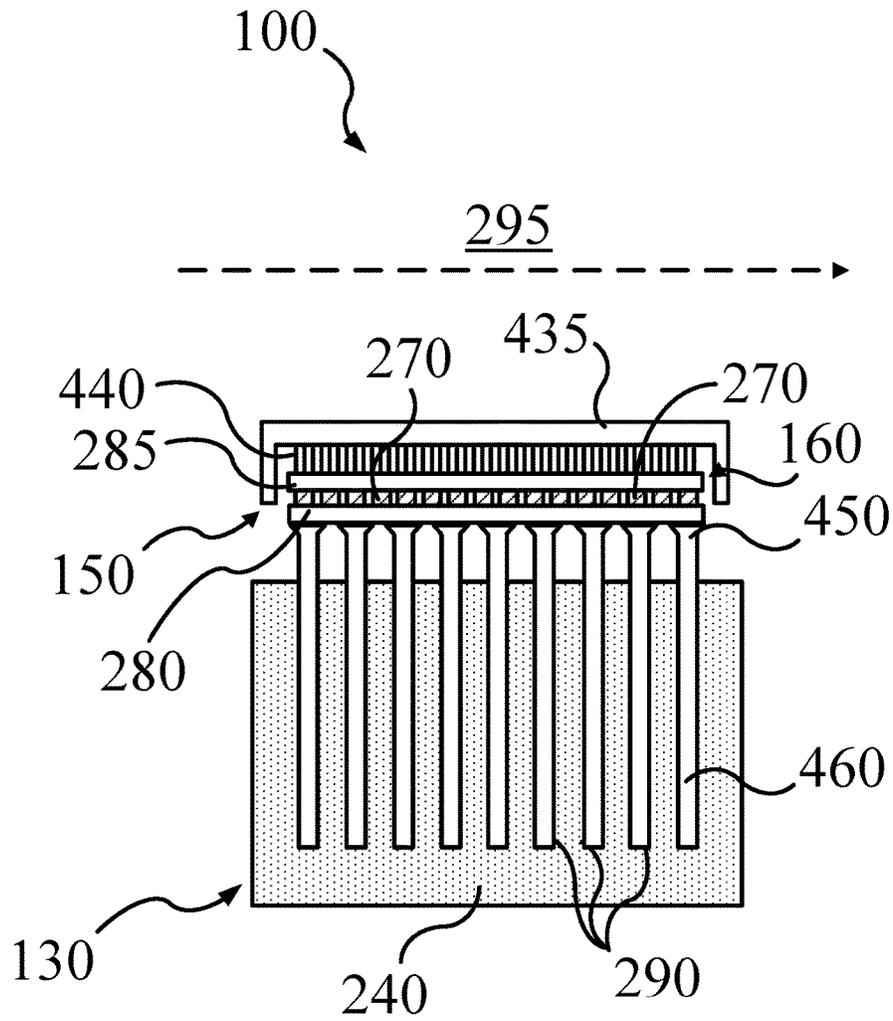


Figure 4a

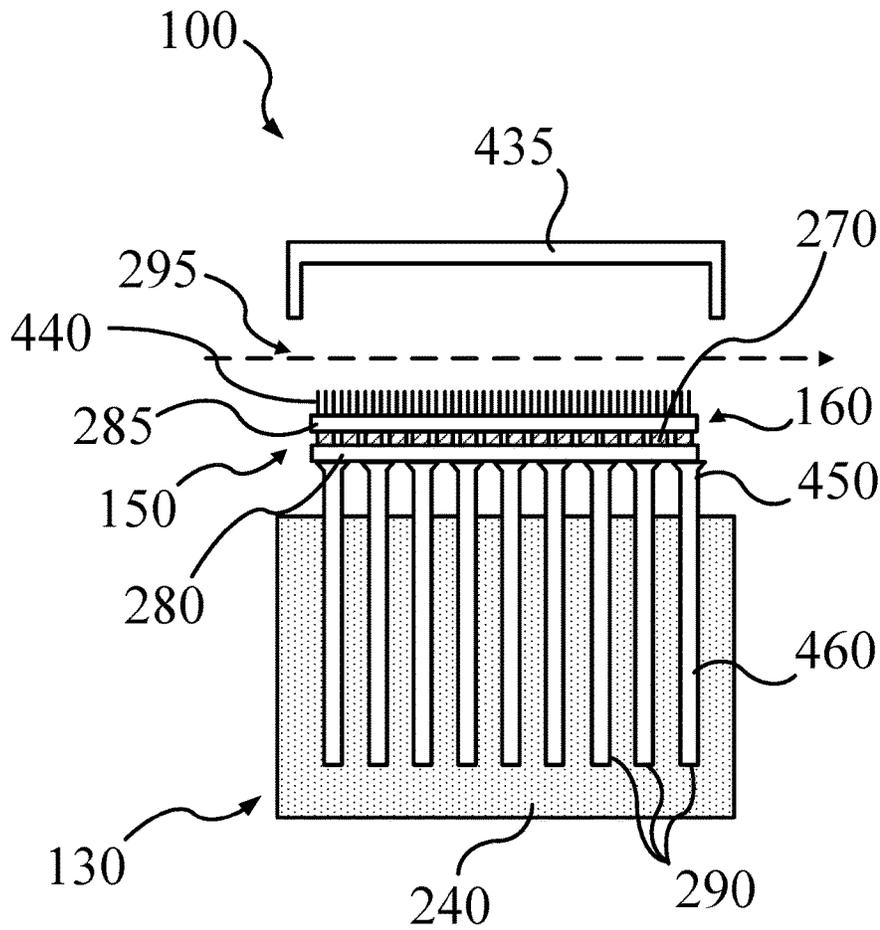


Figure 4b

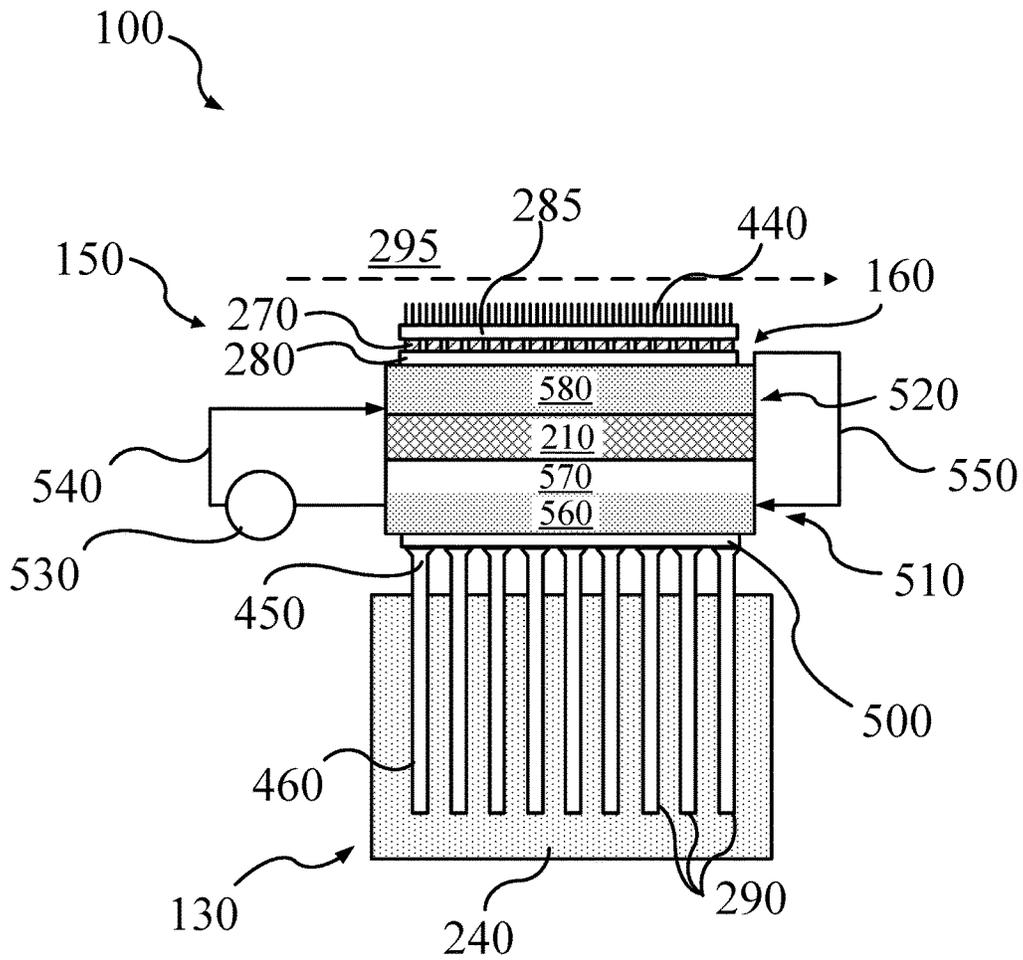


Figure 5

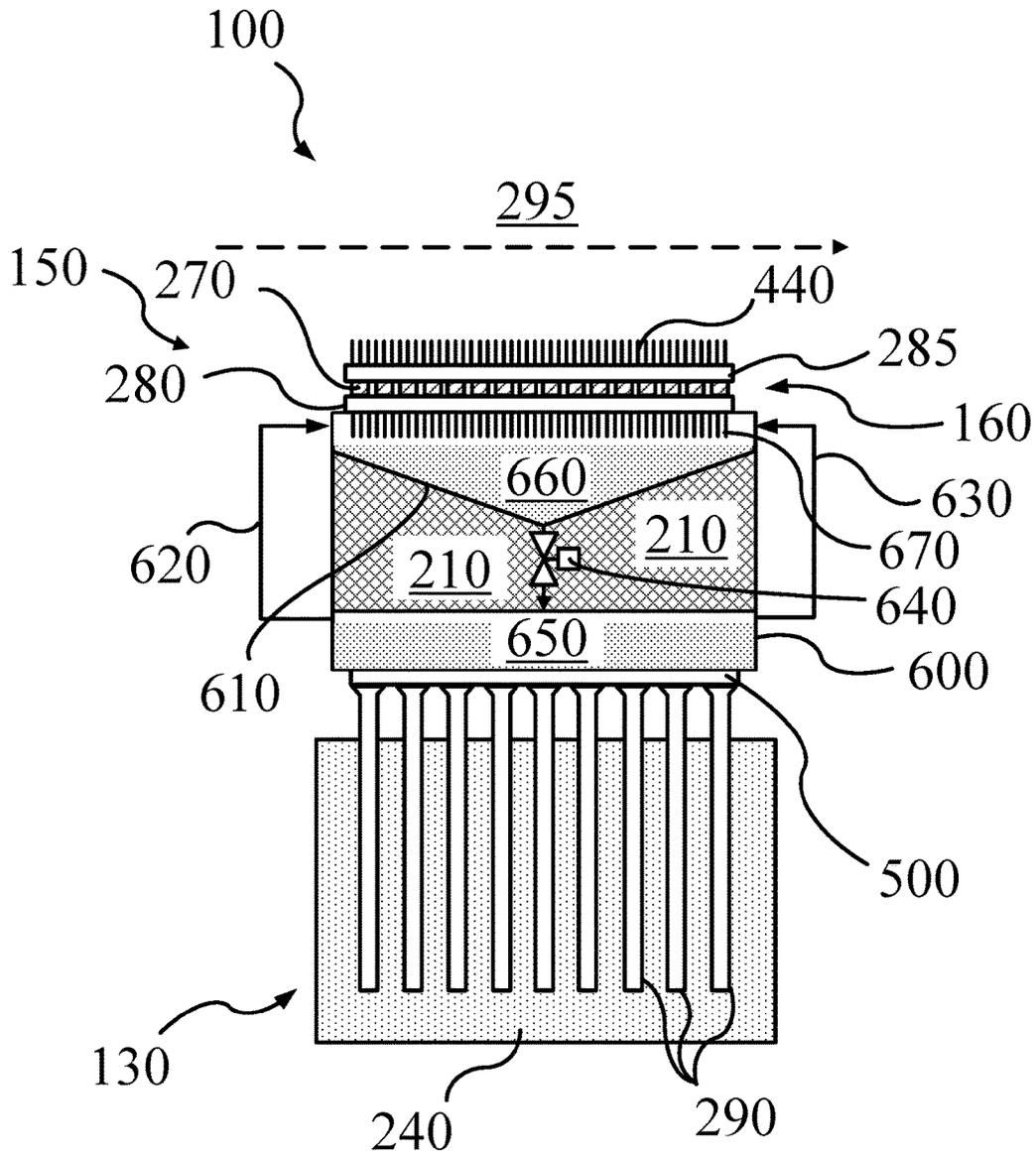


Figure 6

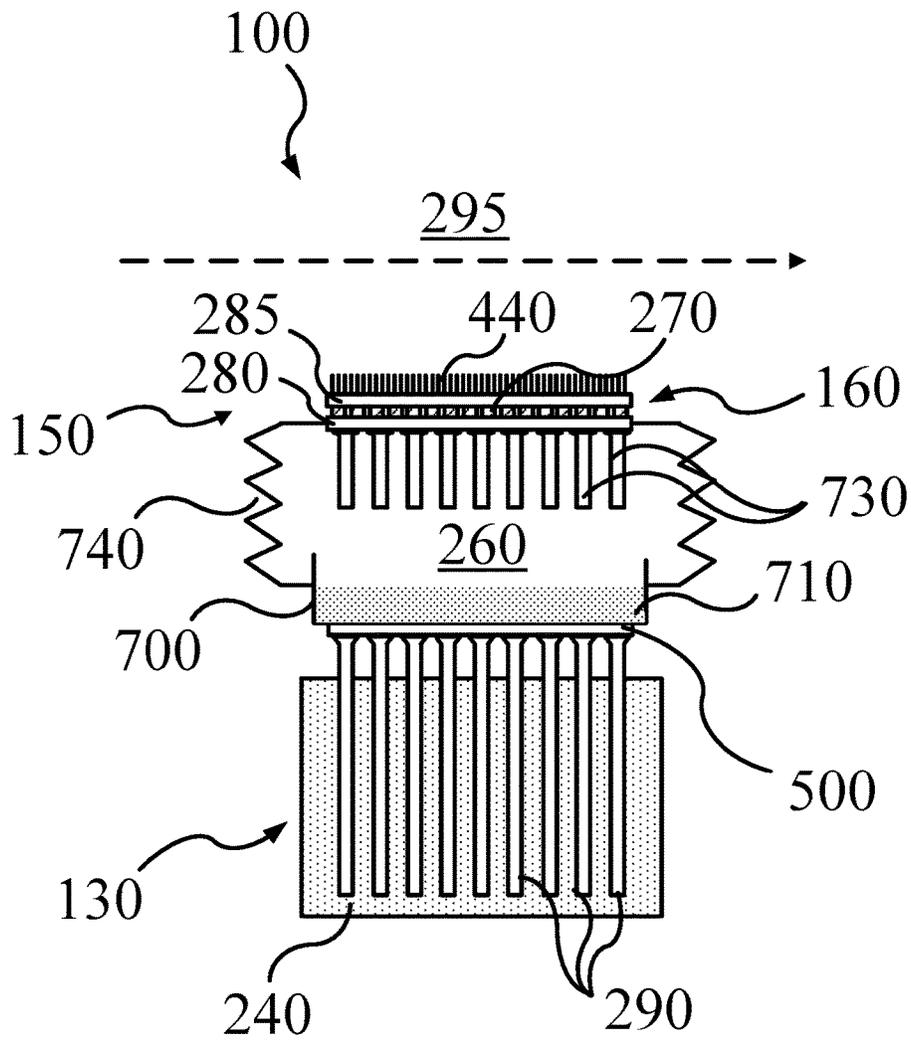


Figure 7a

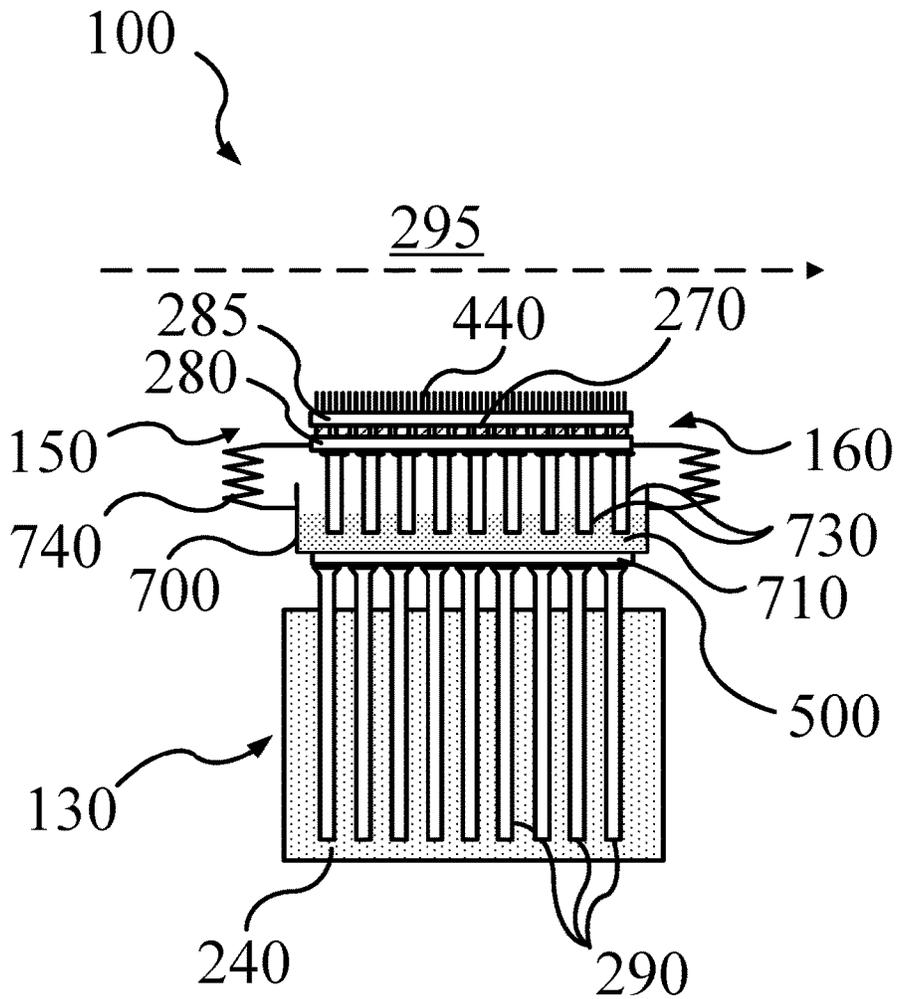


Figure 7b

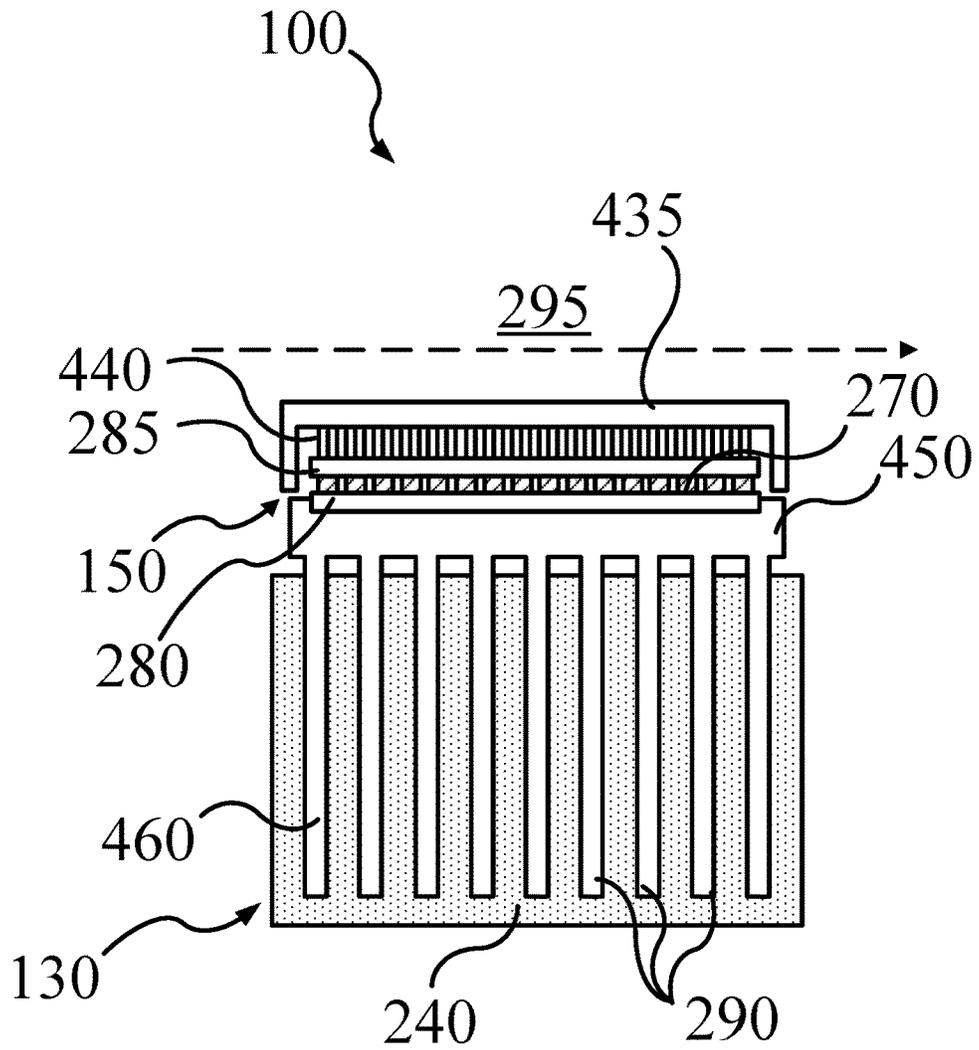


Figure 8a

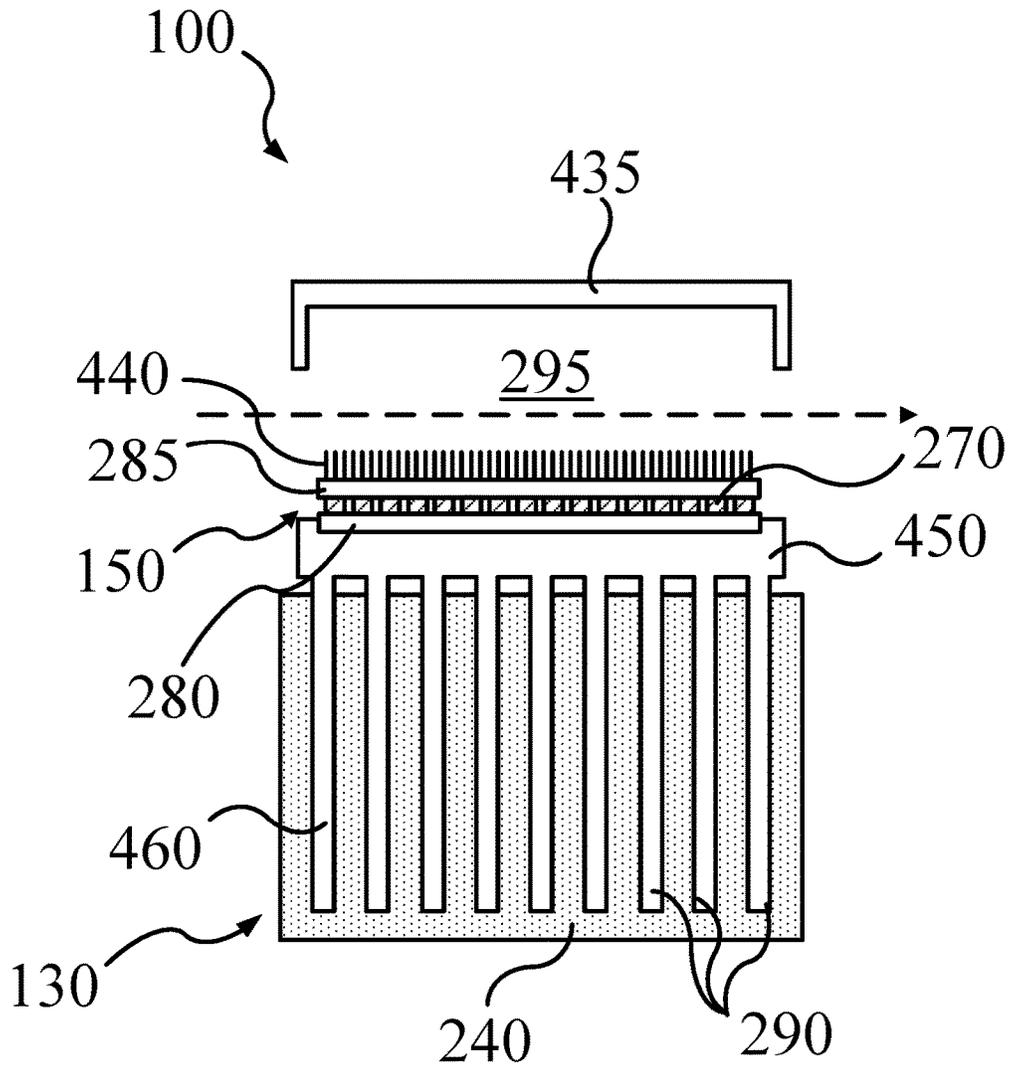


Figure 8b

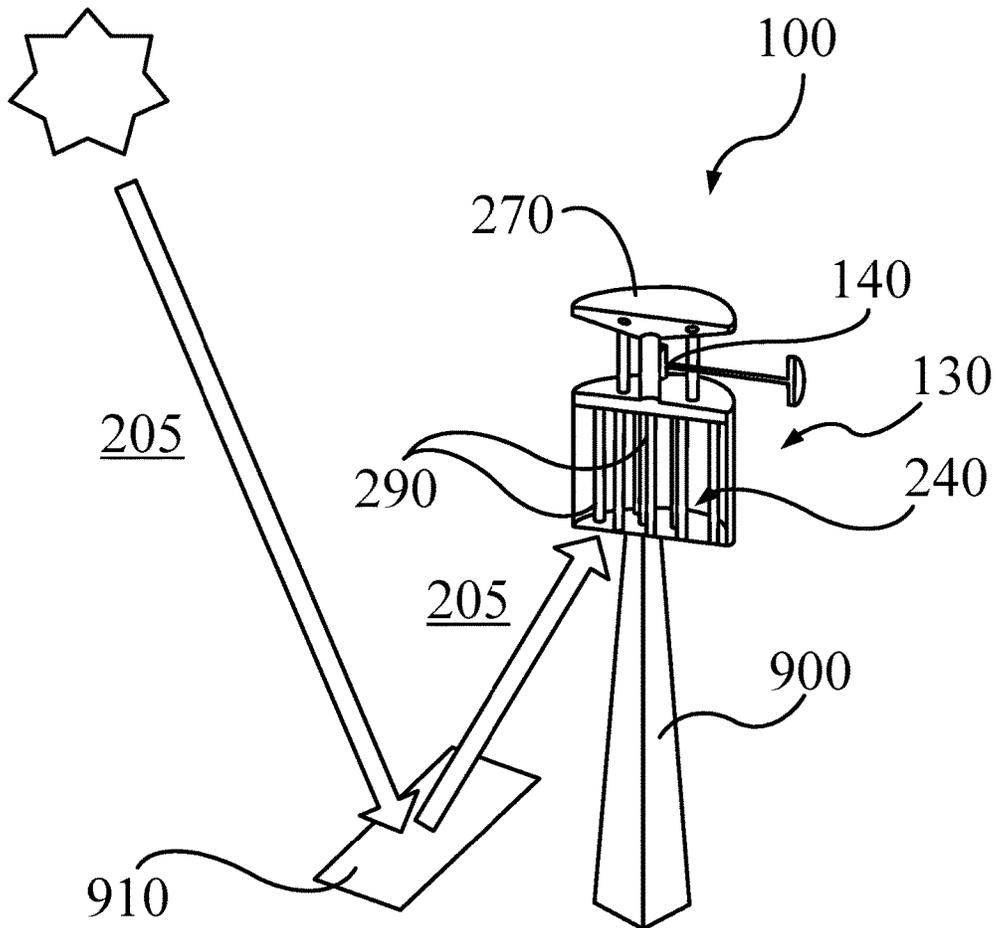


Figure 9

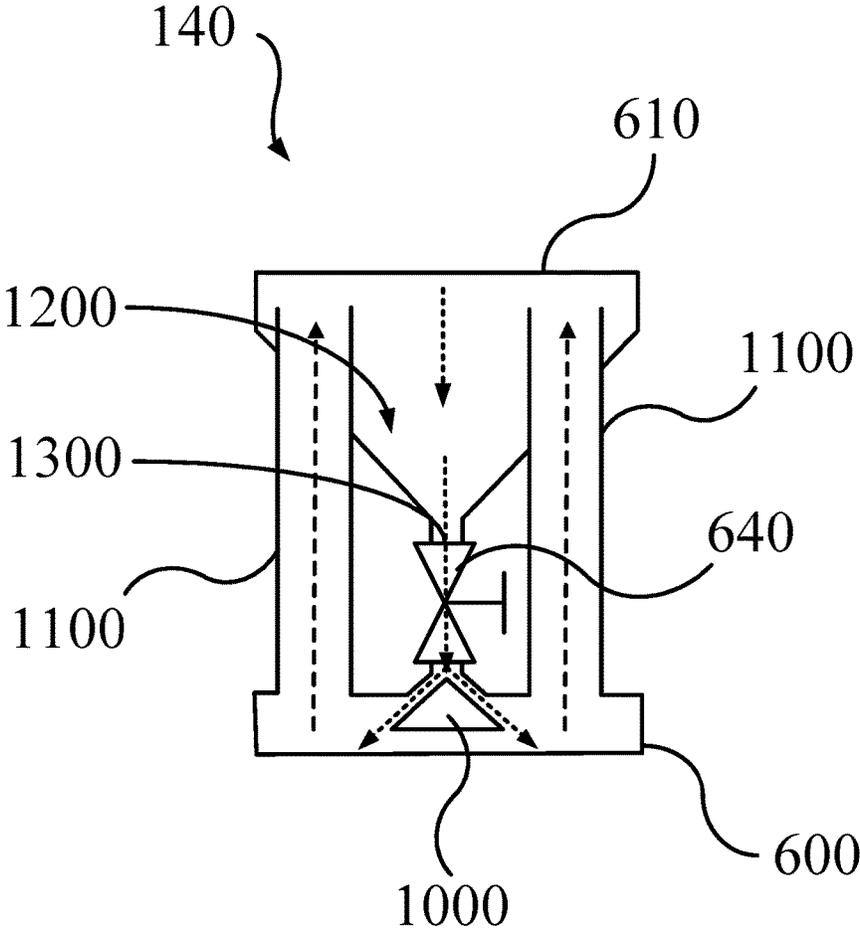


Figure 10a

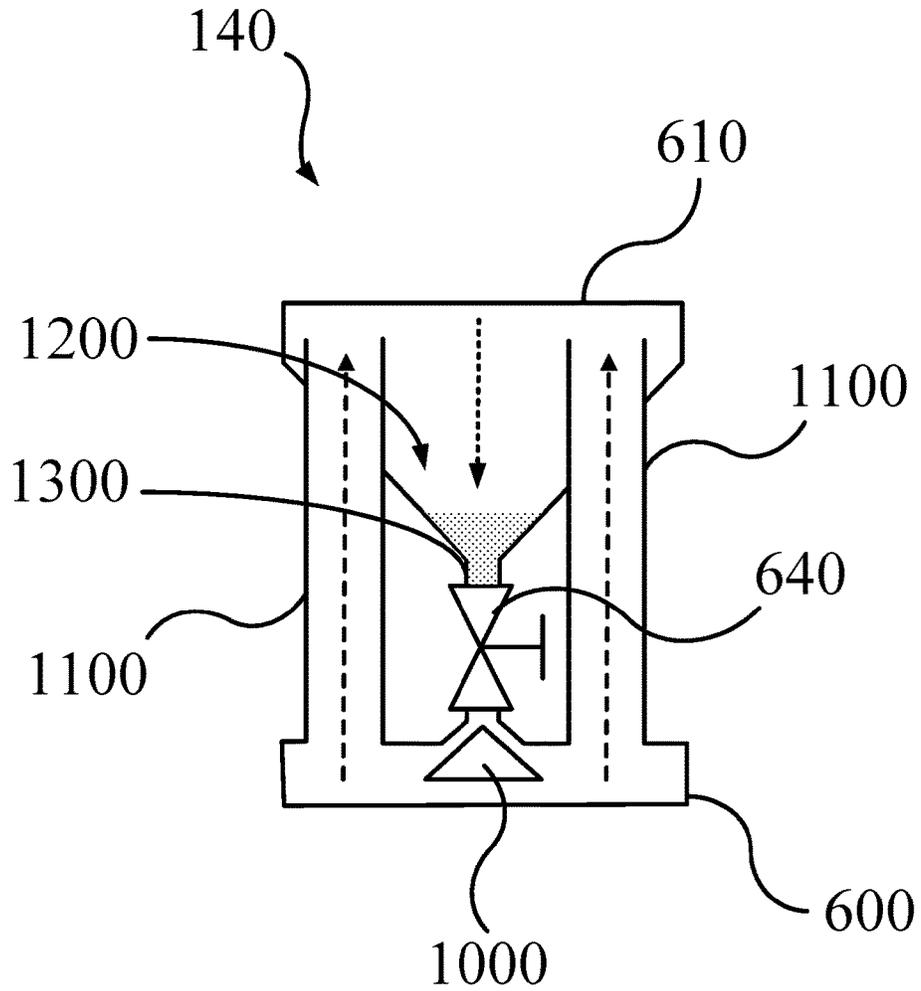


Figure 10b

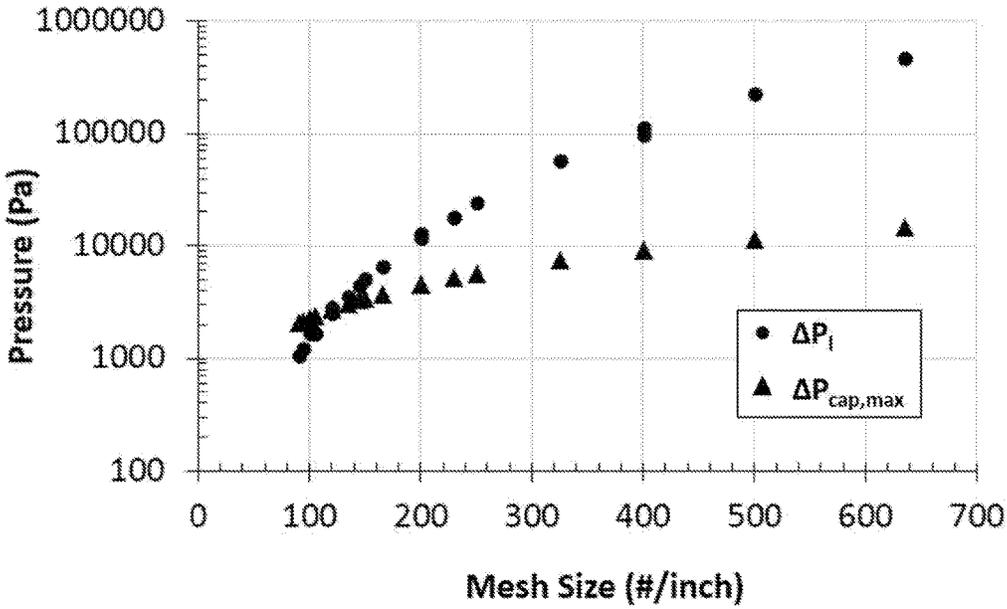


Figure 11

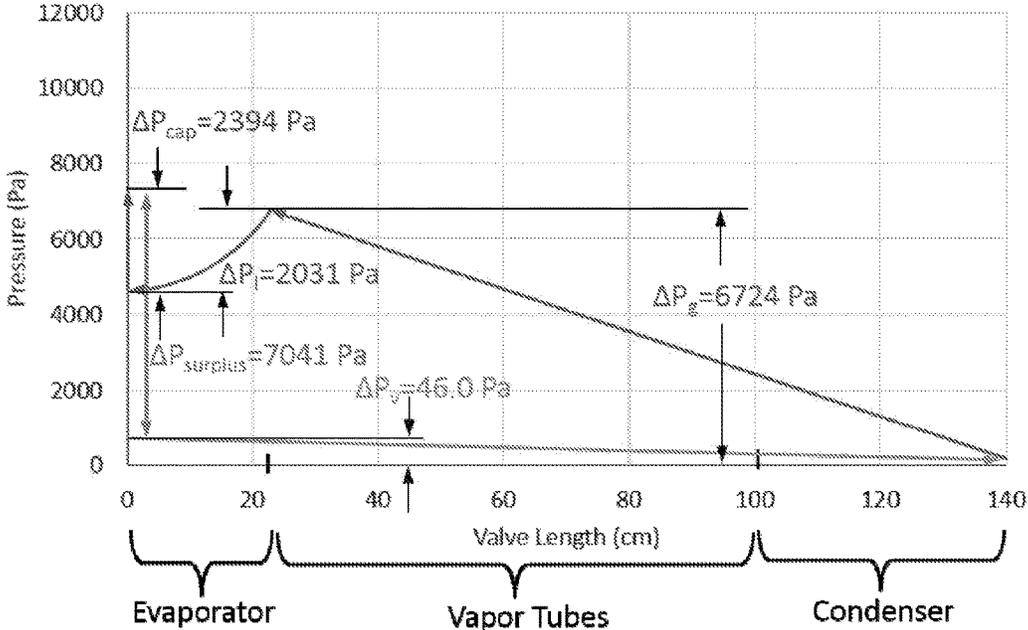


Figure 12

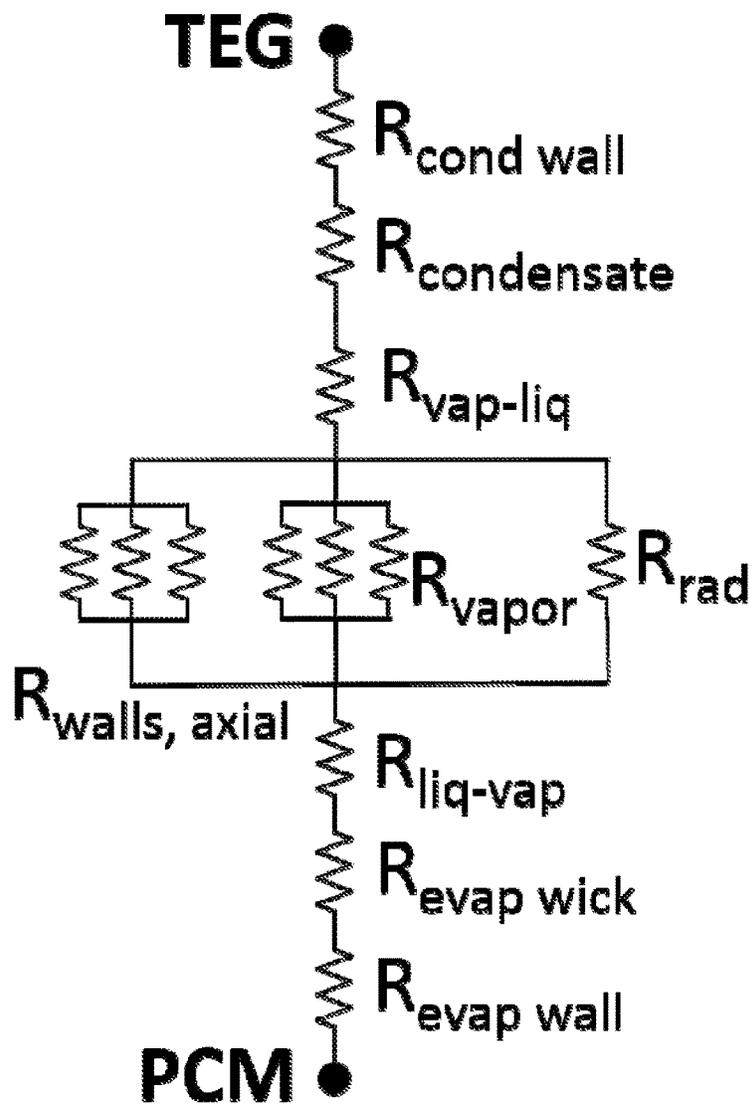


Figure 13

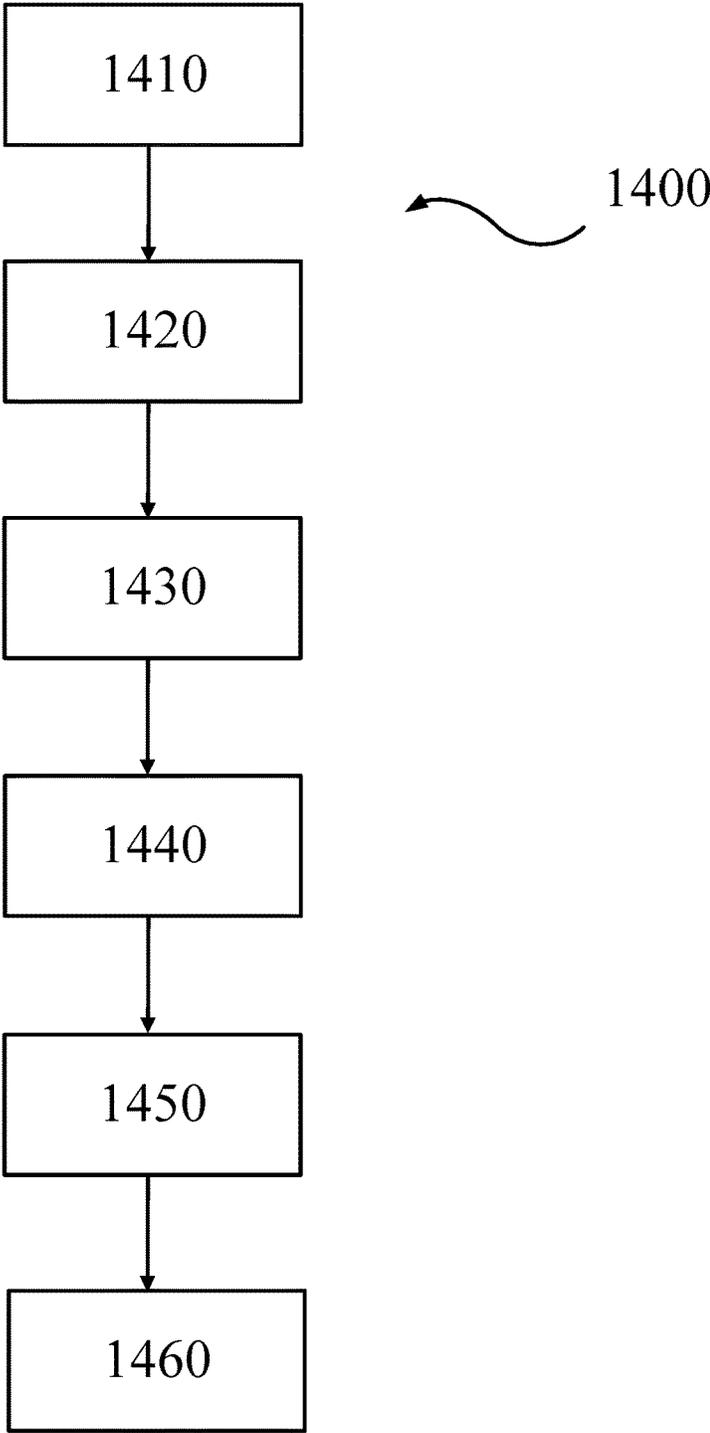


Figure 14

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**SOLAR THERMOELECTRICITY VIA  
ADVANCED LATENT HEAT STORAGE****CROSS-REFERENCE TO RELATED  
APPLICATIONS**

This application claims the benefits of U.S. Provisional Application Nos. 62/240,342 and 62/315,923 filed Oct. 12, 2015 and Mar. 31, 2016 respectively, the contents of which are incorporated herein by reference in their entirety.

**CONTRACTUAL ORIGIN**

The United States Government has rights in this invention under Contract No. DE-AC36-08GO28308 between the United States Department of Energy and the Alliance for Sustainable Energy, LLC, the Manager and Operator of the National Renewable Energy Laboratory.

**BACKGROUND**

The generation of electricity from solar energy has typically been accomplished via two technologies: photovoltaics (PV) and concentrated solar power (CSP). PV modules are highly scalable solid-state devices with few moving parts (e.g. the mechanics associated with tracking the sun). However, because sunlight is directly converted to electricity, intermittent clouds cause variability in power generation. Overcoming these short-term variations, as well as shifting production times from peak sunlight hours (around noon) to peak demand hours (evening), requires the development of energy storage systems that can be incorporated into solar-based energy production systems. The most common solution for PV is costly energy storage batteries. In contrast, CSP offers comparatively low-cost thermal energy storage solutions. However, such CSP thermal energy technologies also require the use of large turbines and the pumping of large quantities of heat transfer fluids, resulting in relatively high operation and maintenance (O&M) costs. Thus, there remains a need for a cost-effective technology that can collect and store energy and easily convert the stored energy to electricity when needed, from solar and other transient energy sources. The present disclosure offers an alternative means of generating electricity from such transient energy sources that has limited moving parts, and is also modular, scalable, and potentially cost effective.

**SUMMARY**

An aspect of the present disclosure is a system that includes a thermal valve having a first position and a second position, a heat transfer fluid, and an energy converter where, when in the first position, the thermal valve prevents the transfer of heat from the heat transfer fluid to the energy converter, and when in the second position, the thermal valve allows the transfer of heat from the heat transfer fluid to the energy converter, such that at least a portion of the heat transferred is converted to electricity by the energy converter.

In some embodiments of the present disclosure, the system may further include a phase change material (PCM) configured to receive thermal energy, where the PCM may be in thermal communication with the heat transfer fluid, such that when the thermal valve is in the second position, at least a portion of the thermal energy may be transferred from the PCM to the heat transfer fluid. In some embodiments of the present disclosure, the system may further

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include a receiver configured to receive the thermal energy, such that the PCM may be in thermal communication with the receiver, and the thermal energy may include at least one of solar energy, geothermal energy, and/or energy from industrial sources.

An aspect of the present disclosure is a system that includes a first container having a first internal volume at least partially defined by a wall, a mechanical valve having a closed position and an open position, and a first heat transfer fluid positioned within the first internal volume. When in the closed position, the mechanical valve separates the first internal volume into a first portion and a second portion that includes the wall, such that the first heat transfer fluid cannot be transported between the first portion and to the wall, and when in the open position, the mechanical valve provides a channel that allows the first heat transfer fluid to move from the first portion to the wall such that heat is transferred from the first heat transfer fluid to the wall. In some embodiments of the present disclosure, the first container may include a vertically oriented cylinder and/or a duct. In some embodiments of the present disclosure, the system may further include a wicking structure positioned within the first internal volume of the cylinder.

In some embodiments of the present disclosure, the system may further include an energy converter in thermal communication with the wall such that, when the mechanical valve is in the open position, a portion of the heat transferred from the first heat transfer fluid to the wall may be transferred to the energy converter, which may convert the portion of the heat transferred to electricity. In some embodiments of the present disclosure, the energy converter may include at least one of a thermoelectric generator and/or a heat cycle. In some embodiments of the present disclosure, the heat cycle may include at least one of a Stirling Cycle, a Ranking Cycle, and/or a Brayton Cycle. In some embodiments of the present disclosure, the system may further include a first heat transfer plate positioned between the wall and the energy converter, in thermal communication with both. In some embodiments of the present disclosure, the system may further include a second heat transfer fluid, where the energy converter may include a first surface and a second surface, the first surface may be in thermal communication with the wall, and the second surface may be in thermal communication with the second heat transfer fluid. In some embodiments of the present disclosure, the second heat transfer fluid may include air. In some embodiments of the present disclosure, the air may be at a temperature between about 0° C. and about 100° C. In some embodiments of the present disclosure, the system may further include a plurality of fins physically attached to the second surface of the energy converter.

In some embodiments of the present disclosure, the system may further include a phase change material (PCM) configured to receive thermal energy, where the PCM may be in thermal communication with the heat transfer fluid, and when the mechanical valve is in the open position, at least a portion of the thermal energy may be transferred from the PCM to the first heat transfer fluid. In some embodiments of the present disclosure, the system may further include a receiver configured to receive the thermal energy, where the PCM may be in thermal communication with the receiver, and the thermal energy may include at least one of solar energy, geothermal energy, and/or energy from industrial sources. In some embodiments of the present disclosure, the system may further include a second heat transfer plate positioned between the receiver and the PCM, in thermal communication with both. In some embodiments of

the present disclosure, the system may further include a second container having a second internal volume, where the PCM may be positioned within the second internal volume, and the first container may be at least partially immersed in the PCM. In some embodiments of the present disclosure, the first heat transfer fluid may have a boiling point between about 500° C. and about 800° C. In some embodiments of the present disclosure, the boiling point may be at a pressure less than 1 atmosphere. In some embodiments of the present disclosure, the first heat transfer fluid may include at least one of sodium and/or a sodium-potassium eutectic material. In some embodiments of the present disclosure, the sodium-potassium eutectic material may include NaK. In some embodiments of the present disclosure, the PCM may undergo a reversible liquid-to-solid phase transition at a temperature between about 500° C. and about 800° C. In some embodiments of the present disclosure, the PCM may include at least one of aluminum and/or an aluminum alloy.

An aspect of the present disclosure is a method that includes receiving thermal energy from an energy source, transferring the thermal energy to a phase change material (PCM), delivering at least a portion of thermal energy from the PCM to a heat transfer fluid, transferring at least a fraction of the portion of thermal energy from the heat transfer fluid to an energy converter, and converting at least a portion of the fraction of the portion of thermal energy to electricity. In some embodiments of the present disclosure, the method may further include, after the transferring the thermal energy to the PCM, storing the thermal energy in the PCM for a period of time before the delivering.

BRIEF DESCRIPTION OF THE DRAWINGS

Exemplary embodiments are illustrated in referenced figures of the drawings. It is intended that the embodiments and figures disclosed herein are to be considered illustrative rather than limiting.

FIG. 1 illustrates a power system, according to some embodiments of the present disclosure.

FIG. 2 illustrates a power system utilizing mechanical valves as thermal valves, according to some embodiments of the present disclosure.

FIGS. 3a and 3b illustrate a power system utilizing, among other things, insulating blocks as a thermal valve, according to some embodiments of the present disclosure.

FIGS. 4a and 4b illustrate a power system utilizing a thermal cover as a thermal valve, according to some embodiments of the present disclosure.

FIG. 5 illustrates a power system utilizing, among other things, a circulating heat transfer liquid between two heat exchangers as a thermal valve, according to some embodiments of the present disclosure.

FIG. 6 illustrates a power system utilizing, among other things, a circulating heat transfer fluid between an evaporator and a condenser as a thermal valve, according to some embodiments of the present disclosure.

FIGS. 7a and 7b illustrate a power system utilizing, among other things, a moveable second set of heat pipes and a heat transfer liquid as a thermal valve, according to some embodiments of the present disclosure.

FIGS. 8a and 8b illustrate another embodiment of the example shown in FIGS. 4a and 4b, with another configuration for a condensing zone, according to some embodiments of the present disclosure.

FIG. 9 illustrates an example of a proposed 3 kW dispatchable PCM/TEG thermal energy storage and power generation system, according to some embodiments of the present disclosure.

FIGS. 10a and 10b illustrate a thermal valve in the “on” state (a) and in the “off” state (b), according to some embodiments of the present disclosure.

FIG. 11 illustrates data showing the relationship between the viscous liquid pressure losses and corresponding capillary pumping pressure of various woven mesh sizes, according to some embodiments of the present disclosure.

FIG. 12 illustrates a plot showing the liquid and vapor pressures along the length of the thermal valve, according to some embodiments of the present disclosure.

FIG. 13 illustrates a thermal resistance network showing each component of a thermal valve, according to some embodiments of the present disclosure.

FIG. 14 illustrates a method for receiving, storing, and converting thermal energy to electricity, according to some embodiments of the present disclosure.

REFERENCE NUMBERS

- 100 . . . power system
- 110 . . . energy source
- 120 . . . receiver
- 130 . . . thermal storage system
- 140 . . . thermal valve
- 150 . . . energy converter
- 160 . . . heat exchanger
- 190 . . . electricity
- 200 . . . aperture
- 205 . . . light
- 210, 230 . . . insulation
- 220 . . . reflecting surface
- 240 . . . phase change material (PCM)
- 250 . . . interface
- 260 . . . empty volume
- 270 . . . thermoelectric generator (TEG)
- 280 . . . first heat transfer plate
- 285 . . . second heat transfer plate
- 290 . . . heat pipe
- 295 . . . airflow
- 300 . . . condensing heat transfer fluid
- 310 . . . vaporizing heat transfer fluid
- 400 . . . optics
- 410 . . . insulating blocks
- 420 . . . ram
- 430 . . . insulating blocks
- 435 . . . thermal cover
- 440 . . . first fins
- 450 . . . condensing zone
- 460 . . . vaporizing zone
- 500 . . . third heat transfer plate
- 510 . . . second heat exchanger
- 520 . . . third heat exchanger
- 530 . . . pump
- 540 . . . liquid supply line
- 550 . . . liquid return line
- 560 . . . first liquid volume
- 570 . . . empty volume
- 580 . . . second liquid volume
- 600 . . . evaporator
- 610 . . . condenser
- 620 . . . first vapor supply line
- 630 . . . second vapor supply line
- 640 . . . mechanical valve

- 650 . . . first fluid volume
- 660 . . . second fluid volume
- 670 . . . second tins
- 700 . . . vessel
- 710 . . . heat transfer liquid
- 730 . . . second heat pipes
- 740 . . . bellows seal
- 900 . . . tower
- 910 . . . heliostat
- 1000 . . . diverter cone
- 1100 . . . vapor tube
- 1200 . . . condensate funnel
- 1300 . . . liquid return tube
- 1400 . . . method
- 1410 . . . receiving thermal energy
- 1420 . . . transferring thermal energy
- 1430 . . . storing thermal energy
- 1440 . . . delivering thermal energy
- 1450 . . . transferring thermal energy
- 1460 . . . converting thermal energy

DETAILED DESCRIPTION

The present disclosure relates to systems and methods for storing thermal energy for eventual conversion of the thermal energy to electricity. FIG. 1 illustrates a block diagram of a power system configured to receive energy from an energy source (e.g., solar energy from a heliostat field and/or other thermal energy sources), store the energy as thermal energy, and then convert the thermal energy to electricity when needed, either immediately and/or at some later time. The conversion of the stored thermal energy to electricity is accomplished by the use of a “thermal valve”, which will be described in detail below, in conjunction with phase change materials (PCM) and an energy converter (e.g. a plurality of thermoelectric generators (TEG) or a Stirling engine)

FIG. 1 illustrates the flow of energy through a power system 100 configured to receive and store energy for the immediate and/or eventual production of electricity 190. In this example, the power system 100 has a receiver 120 configured to receive an influx of energy,  $h_m$ , from an energy source 110. For example, the receiver 120 may be a system or device configured to receive solar energy ( $h_m$ ) from a field of heliostats (the energy source 110). Alternatively, the energy source 110 may be other relatively high temperature energy sources, including geothermal sources and/or various industrial sources (e.g. high temperature exhaust streams). In addition, the receiver 120 may be configured to transfer at least a portion of the energy received,  $h_m$ , to a thermal storage system 130, where the energy transferred,  $h_1$ , may be stored as thermal energy. As will be described below, this stored energy may be stored indefinitely until needed (e.g. evening peak demand) and converted to electricity 190 by an energy converter 150. Or, alternatively, the thermal energy,  $h_1$ , transferred to the thermal storage system 130 may be converted immediately to electricity 190 by the energy converter 150. In some embodiments, even excess electrical energy (e.g. during periods of low use) may be converted to heat for temporary storage and later converted back to electrical energy (e.g. during peak demand periods). Transfer of energy,  $h_2$  and  $h_3$ , from the thermal storage system 130 to the energy converter 150 is controlled and/or regulated by a thermal valve 140.  $h_3$  may be less than or equal to  $h_2$ , depending on thermal losses to the environment. Examples of energy converters 150 suitable for some embodiments of the present disclosure include various heat engines (heat cycles) and/or TEGs. Examples of heat cycles that may be

used in some embodiments of the present disclosure include the Stirling Cycle, the Rankine Cycle, the Brayton Cycle, and/or any other heat cycle.

The process of transferring energy,  $h_1$ , from the receiver 120 to a thermal storage system 130 is described herein as “charging” the power system 100 with thermal energy. A thermal storage system 130 may have a maximum energy storage capacity and/or a corresponding maximum operating temperature. For example, a thermal storage system 130 may include a fixed mass of a phase change material (not shown in FIG. 1), where the system’s energy storage capacity is defined as at least the sum of the sensible heat needed to heat the phase change material (PCM) from a starting temperature to the PCM’s melting point, plus the latent heat required to fully melt the entire mass of the PCM. Thus, a power system 100 may be considered to be fully charged when the PCM contained within a thermal storage system 130 has been completely melted, with minimal or no additional energy input to raise the temperature of the PCM above its melting point temperature. In this example, the maximum operating temperature may be defined as the melting temperature of the PCM. In other cases, the PCM may be heated to a temperature higher than its melting point, where the thermal storage system’s maximum operating temperature may be higher than the melting point temperature of the PCM. Thus, a thermal storage system 130 may reach maximum operating temperatures ( $T_H$ ) corresponding to temperatures from about 500° C. to about 800° C., depending at least upon the PCM chosen. Examples of phase change materials that may be used in a thermal storage system 130 include aluminum and/or aluminum alloys, and chloride, fluoride, and/or sulfate salts. In some embodiments of the present disclosure, the maximum operating temperature ( $T_H$ ) may be between about 300° C. and about 1000° C.

Due to such relatively high operating temperatures, a thermal storage system 130 may require at least some insulation (not shown) to prevent or minimize energy losses to the environment; e.g. due to conductive, radiant, and/or convective losses. However, a thermal storage system’s high operating temperature also enables the efficient use of a heat engine. The upper limit for the conversion of energy by a heat engine is the Carnot efficiency, as defined by Equation A below, where  $T_H$  corresponds to a relatively high temperature for the “hot-side” of a heat engine, and  $T_C$  corresponds to a relatively low temperature for the “cold-side” of a heat engine. Equation A illustrates that higher temperature differentials,  $\Delta T = T_H - T_C$ , across the energy converter result in higher conversion efficiencies;

$$\eta = \frac{T_H - T_C}{T_H} \tag{A}$$

Equation A shows that as the ratio of  $T_C$  to  $T_H$  decreases, a heat engine’s efficiency for converting thermal energy to electricity,  $\eta$ , increases ( $\eta$  is also equal to  $1 - h_4/h_3$ ). Thus, placing the hot-side (or first side) of a plurality of TEGs or a Stirling engine in thermal communication with a thermal storage system 130 containing a PCM at a relatively high operating temperature (e.g. melting temperature), and placing the cold-side (or second side) of the plurality of TEGs or a Stirling engine in thermal communication with a heat exchanger 160 operated at a relatively low temperature, may result in a high heat flux through the energy converter and high conversion efficiencies by the heat engine (e.g. conversion of thermal heat to electricity).

A heat exchanger **160** may include a conductive material (e.g. solid metal) positioned with a first side in contact with an energy converter **150** (e.g. the cold-side of a TEG or TEG module), and a second side positioned within the flow of a cooling fluid (a heat transfer fluid; not shown). The cooling fluid, for example a low temperature gas, may act as a heat sink for the removal of any heat not converted to electricity by the TEGs. For example, a heat exchanger **160**, may be a conductive slab and/or layer (e.g. a solid metal), with a first surface of the conductive layer placed in direct contact with the cold-sides of a bank of TEGs, and a second surface placed within the flow of a relatively colder air stream (not shown). In such examples, a cold air stream may have a bulk temperature from about  $-20^{\circ}\text{C}$ . to about  $100^{\circ}\text{C}$ . Thus, the cold-side temperature,  $T_c$ , of a TEG may be about  $-20^{\circ}\text{C}$ . to about  $100^{\circ}\text{C}$ . A heat exchanger **160** may include various features to promote and/or maximize the transfer of energy from the heat exchanger **160** to the cooling fluid; e.g. by maximizing the surface area and/or heat transfer coefficient of the heat exchanger. One example includes increasing a heat exchanger's surface area in contact with a cooling fluid by the use of fins and/or other surface area extensions attached to a conductive layer. Other suitable heat exchanger **160** configurations may be implemented to increase the outside heat transfer coefficient of the heat exchanger **160**.

Given the potentially high temperature difference between the hot-side,  $T_H$ , and the cold-side,  $T_C$ , of an energy converter **150**, the driving force for heat transfer from a thermal storage system **130** to the energy converter **150**, and then through the energy converter **150** to a heat exchanger **160**, may be relatively high. In some cases,  $\Delta T = T_H - T_C$  may be a  $\Delta T$  of about  $400^{\circ}\text{C}$ . to a  $\Delta T$  of about  $800^{\circ}\text{C}$ . A large  $\Delta T$  driving force for heat transfer may be desirable when discharging the thermal energy from the thermal storage system **130** to the energy converter **150**. However, for a power system **100** to function as desired, e.g. to collect and/or store energy (e.g. during periods of sunlight) and later generate electricity when needed (e.g. during periods of peak demand in the evenings), a robust and reliable switching mechanism is desirable. Such a switching mechanism should be able to switch between a first mode of charging and/or storing thermal energy, to a second mode of discharging the thermal energy to generate electricity, and back again (reversible), as many times as needed. A thermal valve **140**, as described herein, provides this functionality.

FIG. 1 illustrates an example of a thermal valve **140** as a mechanical on/off valve. This is because a thermal valve **140**, as described herein, has at least two positions, a first "open" position and a second "closed" position, similar to a simple mechanical valve. In the "closed" position, a thermal valve **140** is configured to thermally isolate the thermal storage system **130** from the energy converter **150** (e.g. TEGs or a Stirling engine). For a system storing thermal energy at relatively high temperatures, a thermal valve **140** in the "closed" position may be configured to minimize heat transfer from the thermal storage system **130** to the energy converter **150**. A thermal valve **140** in the "open" position may be configured to maximize conductive, radiant, convective, and/or any other means of heat transfer from the thermal storage system **130** to the energy converter **150**. So, although FIG. 1 illustrates a simple mechanical valve as the thermal valve **140**, some embodiments of a thermal valve **140** may include various elements and features working together to both retain thermal energy within the thermal storage system **130** (e.g. when charging), and also efficiently transfer this thermal energy to the energy converter **150**

when electricity generation is needed (e.g. when discharging). However, in the case where a simple mechanical valve is incorporated into the thermal valve **140**, any suitable (e.g. insulated) mechanical valve, including ball valves, gate valves, and/or plug valves may be used.

In summary, referring again to FIG. 1, a power system **100** for receiving and storing energy and converting energy to electricity **190** may include a receiver **120** configured to receive energy,  $h_{in}$ , from an energy source **110**. The receiver **120** may transfer at least a portion of the energy received,  $h_1$ , to a thermal storage system **130**, where it may be stored for later use and/or immediately transferred to an energy converter **150** for the production of electricity **190**. The transfer of energy from the thermal storage system **130** to the energy converter **150** is controlled by a thermal valve **140**, where the thermal valve **140** has an "open" position that enables the flow of energy,  $h_2$  and  $h_3$ , from the thermal storage system **130** to the energy converter **150**, and a "closed" position that prevents the flow of energy,  $h_2$  and  $h_3$ , from the thermal storage system **130** to the energy converter **150**. When in the "open" position, energy transfer may be driven by the temperature differential between the thermal storage system **130** at a relatively high operating temperature, and a heat sink (e.g. the external environment) at a relatively low temperature. The transfer of energy to the energy converter **150** may be facilitated by a heat exchanger **160** that maintains an outlet/pathway for any thermal energy not converted to electricity by the energy converter **150**. Thus, the heat exchanger **160** may help maintain the cold-side temperature of the energy converter **150**,  $T_c$ , by providing an outlet for energy not converted to electricity **190**, such that the non-converted energy,  $h_{out}$ , may be ejected from the power system **100** to the outside environment (e.g. heat sink) and/or a cooling heat transfer fluid (not shown).

FIG. 2 illustrates an example of a power system **100** for receiving and storing thermal energy and for converting stored thermal energy to electricity. In this example, a receiver **120** receives light **205** (e.g. electromagnetic radiation) from a heliostat field and/or any other suitable source (not shown). The receiver **120** may be constructed to include insulation **210** in the shape of a dome with a central aperture **200**. The light **205** from the heliostat field may be directed towards the aperture **200** so that at least a portion of the light **205** passes through the aperture **200** to impinge upon a first heat transfer plate **280**. Other internal elements of the aperture **200** may have one or more reflecting surfaces **220**, to maximize the portion of light **205** that impinges upon the first heat transfer plate **280** and/or to minimize energy losses to the environment. For example, a reflecting surface **220** within the aperture **200** may be configured to maximize the reflection of light **205** in the visible, infrared, and/or ultraviolet wavelengths of the solar spectrum from the inside surfaces of the receiver **120**, and/or may be configured to maximize and/or redirect light **205** that has been reflected to the first heat transfer plate **280**. The first heat transfer plate **280** may have a surface and/or coating that maximizes the absorbance of light in the visible, infrared, and/or ultraviolet wavelengths of the solar spectrum, to maximize the transfer of energy from the receiver **120** to the thermal storage system **130**.

Thus, at least a portion of the light **205** absorbed by the first heat transfer plate **280** may be converted to heat and transferred to the thermal storage system **130**. In this example, the thermal storage system **130** includes circular walls made of or encased by insulation or an insulating material **130** and is capped with two heat transfer plates (**280** and **285**) to form an internal volume. As shown in FIG. 2, this

internal volume may be at least partially filled with a phase change material 240. When partially filled with phase change material 240, the phase change material 240 may define an interface 250 (e.g. liquid/gas interface and/or solid/gas interface), which together with the second heat transfer plate 285 defines an empty volume 260 within the thermal storage system 130. Such an empty volume 260 may contain a gas at a pressure ranging from close to full vacuum to several atmospheres of pressure.

The example shown in FIG. 2, shows that a thermal storage system 130 may include a plurality of substantially vertically oriented heat pipes 290, positioned such that a significant portion of the heat pipes' lengths are immersed and/or submerged in the phase change material 240. Further, this example shows a first end of each heat pipe 290 physically attached to the first heat transfer plate 280, and a second end of each heat pipe 290 physically attached to the second heat transfer plate 285, where the second heat transfer plate 285 is in thermal communication with the hot-side of the energy converter 150 (e.g. a TEG module). Each heat pipe 290 may be viewed as a container defined by outside walls, which further define an enclosed, internal space. Although FIG. 2 illustrates these containers in the form of round, cylindrical "pipes", it is to be understood that other three-dimensional shapes and cross-sections are possible for the containers spanning the first heat transfer plate 280 and the second heat transfer plate 285; e.g. triangular, rectangular, square cross-sections of ducts, channels, and/or any other suitable container, etc.

Referring again to the example of FIG. 2, each heat pipe 290 of the thermal storage system 130 contains a heat transfer fluid that undergoes a reversible phase change from liquid-to-gas, within the inside volume of each heat pipe 290. A wicking structure (not shown) may be added to the interior walls of each heat pipe 290 to promote the flow of the heat transfer fluid, in liquid form, along the long-axis dimension of the each heat pipe 290. The boiling point of the heat transfer fluid may occur at a temperature equal to or less than the melting point temperature of the PCM 240. For example, if the PCM 240 melts/freezes at a temperature  $T_1$ , a heat transfer fluid may be selected for the heat pipes 290 having a boiling-point temperature  $T_2$  that is less than or equal to  $T_1$ . Thus, in some examples, the heat transfer fluid contained within a heat pipe 290 may have a boiling point temperature from about 100° C. to about 800° C., at pressures ranging from about 1 atmosphere or less. Some examples of suitable heat transfer fluids for the heat pipes 290 used include sodium and/or potassium for the upper end of the temperature range, and water, methanol, and naphthalene for lower operating temperatures.

FIG. 2 illustrates a simple embodiment of a thermal valve 140, in the form of an on/off mechanical block valve. In this example, such a thermal valve is positioned to divide its associated heat pipe 290 into a first section, which is substantially in direct contact with (e.g. submerged) the PCM 240, from a second section of heat pipe 290 that is positioned substantially within the empty volume 260 of the thermal storage system 130. As described above, each thermal valve 140, in this case each mechanical valve, has at least two positions. The first position corresponds to an "open" position in which each thermal valve 140 allows substantially unrestricted flow of mass and/or energy between the first section of its corresponding heat pipe and the second section of the heat pipe. Thus, while in the "open" position, each thermal valve 140 allows the flow of heat transfer fluid, as condensate and/or vapor, between the two sections of its corresponding heat pipe 290. The second

position corresponds to a "closed" position in which each thermal valve 140 blocks and/or restricts the flow of mass and/or energy between the two sections of its respective heat pipe 290.

As each heat pipe 290 illustrated in FIG. 2 is physically connected to both the first heat transfer plate 280 and the second heat transfer plate 285, each heat pipe 290 is also in thermal communication with both heat plates (280 and 285). Thus, each heat pipe 290 is configured to achieve at least two tasks. First, each heat pipe 290 assists with charging the thermal storage system 130 with thermal energy by enabling the charging process to occur faster and/or by enabling more effective heating of a larger percentage of the PCM's mass. Second, a heat pipe 290 enables the discharge of thermal energy from the thermal storage system 130 to the energy converter 150 to produce electricity when desired. The combination of heat transfer plates (280 and 285) in thermal communication with each heat pipe 290, the PCM 240 in thermal communication with each heat pipe 290, the heat transfer fluid positioned within each heat pipe, and the thermal valves 140 positioned between the high temperature PCM and the energy converter 150 in thermal communication with a relatively low temperature heat sink (e.g. via a heat exchanger 160) function together to enable the on-demand charging and discharging operations of the power system 100.

Referring again to FIG. 2, when charging the thermal storage system 130, with the thermal valves 140 in the "closed" position, at least a portion of the radiant energy from the incoming light 205 may be absorbed as heat by the first heat transfer plate 280 of the receiver 120. A first portion of the resultant heat may be transferred directly to the PCM 240, causing at least a portion of the PCM 240 to heat up and/or melt. A second portion of the heat absorbed may be transferred by the first heat transfer plate 280 to the heat transfer fluid contained within each heat pipe 290, such that at least a portion of the heat transfer fluid heats up and/or vaporizes. During charging there may be significant temperature gradients within the mass of PCM 240 contained within the thermal storage system 130. Thus, vaporized heat transfer fluid may subsequently condense on lower temperature surfaces within the heat pipes 290, for example sections of heat pipe at higher elevations, corresponding to lower temperature PCM 240. As a result, the condensing heat transfer fluid 300 may transfer at least the latent heat of the condensing heat transfer fluid, and possibly some sensible heat, to the lower temperature PCM 240, resulting in a temperature increase to that portion of PCM 240 within the thermal storage system 130. Thus, the repeated vaporization and condensation of the heat transfer fluid within the heat pipes 290 may accelerate the heating of substantially the entire mass of PCM 240 to its melting point temperature, eventually completely melting the entire mass of the PCM 240 to the fully charged state for the thermal storage system 130.

FIG. 2 illustrates the vaporizing heat transfer fluid 310 at the lower end of each heat pipe 290. However, the heat transfer fluid may vaporize at any position along the vertical axis of the heat pipes 290; e.g. vaporization of the heat transfer fluid may occur within a heat pipe at any surface that is at a temperature higher than or equal to the boiling point temperature of the heat transfer fluid, FIG. 2 illustrates the heat transfer fluid condensing at the upper end of each heat pipe 290. However, the heat transfer fluid may condense at any position along the vertical axis of the heat pipes 290; e.g. condensation may occur within a heat pipe 290 at any

surface that is at a temperature lower than or equal to the dew point temperature of the heat transfer fluid.

Referring to FIG. 2, when discharging thermal energy from the thermal storage system 130 to the energy converter 150, the heat pipes 290, thermal valves 140, and related elements (e.g. PCM, heat transfer fluid, heat transfer plates, etc.) also function together. With the thermal valves 140 in the “open” position, vaporized heat transfer fluid may physically access the second heat transfer plate 285 from the hotter zones in the heat pipes 290, below the thermal valves 140. The second heat transfer plate 285, as shown in FIG. 2, may be configured to be in thermal communication with the energy converter 150, which may be in further thermal communication with the heat exchanger 160. The heat exchanger 160 may provide an outlet for unconverted thermal energy to the external environment, and thus, at least partially maintain the high differential temperature that allows the stored energy to be transferred from the thermal storage system 130 to the energy converter 150. As shown in FIG. 2, a heat exchanger 160 may include a first surface in contact with the energy converter 150 (e.g. the cold-side of a TEG module) and a second surface in contact with an airflow 295. The airflow 295 may act as a heat transfer fluid and/or a heat sink to remove heat not converted to electricity by the energy converter 150. This may help maintain a low temperature,  $T_C$ , at the cold-sides of the TEGs, and thus, maintain the relatively high differential temperature useful for the efficient transfer of thermal energy stored in the thermal energy storage system 130 to the energy converter 150 (e.g. TEG module). In the example of FIG. 2, the energy converter 150 is shown to be a plurality of TEG modules 270, but it is to be understood that the TEGs could be replaced by another energy converter, such as a Stirling engine.

Thus, discharging the energy stored in the thermal storage system 130 of FIG. 2 will typically begin with switching the thermal valve(s) 140 from the “closed” position to the “open” position. In the “open” position, mass transfer of the heat transfer fluid may occur between the first portion of each heat pipe and the second portion of each heat pipe. This provides an open channel within each heat pipe 290, which allows for fluid communication between the high temperature zones of each pipe, the heat pipe zones submerged in the PCM 240 at high temperatures, and the low temperature heat pipe zones in thermal communication with the second heat transfer plate 285. This configuration enables the heat transfer fluid, contained within the heat pipes 290, to vaporize in the high temperature zones (vaporization zones), travel through the open thermal valves 140 and condense in the low temperature zones (condensing zones) on surfaces of the second heat transfer plate 285. As a result, at least the latent heat of vaporization, and possibly some of the sensible heat of the heat transfer fluid, may be transferred from the PCM 240 in the thermal storage system 130 to the second heat transfer plate 285. This process may occur continuously until all of the stored energy is transferred from the thermal storage system 130 to the second heat transfer plate 285 and to the energy converter 150 to continuously produce electricity; e.g. until substantially all of the PCM 240 solidifies. In other words, the heat transfer fluid may continue to discharge the thermal energy stored in the thermal storage system 130, by repeated vaporization and condensing, until the temperature of the PCM 240 drops below the boiling point temperature of the heat transfer fluid (for the operating pressure in the heat pipes). Note that while this simple embodiment of a thermal valve 140 can be used to prevent heat flow to the energy converter 150 from a “cold start” (i.e.

the condition in which all of the heat transfer fluid is pooled at the bottom of the pipe in liquid form) and shift the time of electricity production, may not be used to stop the discharge of energy in the system once it has begun. Closing the mechanical valve during discharge may trap some fraction of the heat transfer fluid in the each of the two sections of the pipe, both of which could then continue to transfer heat through their respective sections.

Referring again to FIG. 2, the second heat transfer plate 285 may be at a temperature sufficiently low for the heat transfer fluid to condense on its surface. Condensation of the heat transfer fluid may then create a vacuum that may facilitate further vaporization of the heat transfer fluid. In addition, the surfaces of the second heat transfer plate 285 upon which condensation occurs may be only marginally lower in temperature than the temperature of the PCM 240. Depending on the design, the differential temperature of the PCM 240 melting temperature relative to the operating temperature of the condensing surface of the second heat transfer plate 285 may be a  $\Delta T$  of about  $1^\circ\text{C}$ . to a  $\Delta T$  of about  $30^\circ\text{C}$ . Thus, the second heat transfer plate 285 may provide a hot-side temperature for the energy converter 150,  $T_H$  (see FIG. 1), where  $T_H$  may be very close to the melting temperature of the PCM 240. As shown in FIG. 2, a heat exchanger 160 may be placed in thermal communication with the energy converter 150 to provide a cold-side temperature,  $T_C$  (see FIG. 1), that is significantly lower than  $T_H$ . The resultant large differential temperature  $\Delta T = T_H - T_C$ , may enable the energy converter 150 (e.g. TEGs 270) to convert a significant fraction of the heat transferred from the second heat transfer plate to the energy converter 150 to electricity (see Equation A above).

FIG. 2 illustrates that a heat exchanger 160, in thermal communication with the cold-side of an energy converter 150, may include a plurality of fins positioned within an airflow 295 (heat transfer fluid), where the airflow 295 acts as a heat sink for the removal of any unconverted thermal energy from the power system 100. The fins may increase the surface area of the heat exchanger 160 that is in contact with the airflow 295, thus increasing the heat transfer rate from the heat exchanger 160 to the airflow 295.

In some embodiments of the present disclosure, a thermal valve may have one or more positions in addition to the “open” and “closed” positions. These other positions may be intermediate between the two extremes of “open” and “closed” and may be desirable, for example, to control the flow of mass and/or energy between the sections of a heat pipe. Control of the flow of the heat transfer fluid may be desirable, for example, to control the electricity production rate and/or to avoid thermally shocking an energy converter that is at a relatively cold temperature by suddenly contacting the energy converter with the relatively hot heat transfer fluid. In other words, a thermal valve may have intermediate positions between “open” and “closed” to be able to affect the rate of charging and/or discharging the thermal storage system of a power system. The concept of a thermal valve having more than two positions is applicable for the simple mechanical valve configuration illustrated in FIG. 2, as well as for at least some of the more complicated thermal valve embodiments described below.

FIGS. 3a and 3b illustrate another embodiment of a power system 100 for collecting and storing thermal energy (FIG. 3a), and convening on-demand at least a portion of the stored thermal energy to electricity (FIG. 3b). The example of FIGS. 3a and 3b is inverted relative to the example of FIG. 2, in that the energy received, light 205, is shown entering a receiver 120 at the top of the receiver 120 instead

of at the bottom. However, it should be noted that the power system **100** of FIGS. **3a** and **3b** may be oriented as needed for a particular application, for example, with the receiver **120** positioned at the top of a power system **100**, at the bottom, or tilted with respect to horizontal.

In addition, another notable difference for the example of FIGS. **3a** and **3b** is that the thermal storage system is essentially filled with PCM **240**, with heat pipes **290** positioned essentially completely submerged in the PCM **240**. Unlike the thermal storage system **130** of FIG. **2**, the power system **100** of FIGS. **3a** and **3b** does not contain any significant empty volume within the thermal storage system **130**, except possibly to accommodate volumetric changes upon freezing and melting. Instead, in this embodiment, the thermal storage system **130** has an internal volume that is essentially entirely filled by PCM **240**, with a plurality of heat pipes **290** positioned vertically within the PCM **240**. The internal volume of the thermal storage system **130** is bounded by vertical walls (defining any desirable cross-section shape; e.g. circular, square, or any other suitable shape), a first heat transfer plate **280**, and a second heat transfer plate **285**.

The thermal storage system's internal volume, as shown in FIGS. **3a** and **3b**, may be filled with a phase change material **340** partly because the thermal valve for the embodiment shown in FIGS. **3a** and **3b** are different from those shown in FIG. **2**. Notably, each heat pipe **290** in the power system **100** of FIGS. **3a** and **3b** does not have a mechanical valve configured to separate and/or isolate each heat pipe into sections. Instead, each heat pipe **290** extends uninterrupted from the first heat transfer plate **280**, through the PCM **240**, to the lower positioned second heat transfer plate **285**. This configuration is different because the thermal valve of the power system of FIGS. **3a** and **3b** includes different physical elements that function differently to switch between a "closed" position for charging (FIG. **3a**), and an "open" position for discharging (FIG. **3b**).

FIG. **3a** illustrates the power system **100** during charging and the configuration of the various elements defining the thermal valve when in the "closed" position. As stated above, charging refers to the process of receiving energy from an energy source and storing it within the power system's thermal storage system **130**. The power system **100** of FIGS. **3a** and **3b** utilizes a receiver **120** configured with optics **400** to help concentrate and/or focus incoming light **205** into the receiver **120**. The received light **205** may then pass through an aperture **200** and to impinge upon a first heat transfer plate **280** where at least a portion of the light's energy may be converted to heat, which may then be transferred to the thermal storage system **130**. The aperture **200** may also contain at least a pair of reversibly movable insulating blocks **410**, which when the power system is charging, as shown in FIG. **3a**, are in a retracted position to avoid blocking the incoming light **205**.

As described for the power system illustrated in FIG. **2**, each heat pipe **290** in the power system **100** of FIGS. **3a** and **3b** has an internal volume containing a heat transfer fluid (not shown). Thus, during charging, a first portion of the heat received by the first heat transfer plate **280** may be transferred directly to the PCM **240**, and a second portion of the heat received by the first heat transfer plate **280** may be transferred to the heat transfer fluid contained in the heat pipes **290**. Once the temperature of the heat pipes **290** reaches the boiling point temperature of the heat transfer fluid, the heat transfer fluid will begin to evaporate and condense within the heat pipes **290**. The repeated vaporization and condensation of the heat transfer fluid within the

heat pipes **290** will assist with raising and/or melting substantially all of the PCM **240**.

As described above, this direct transfer of heat into the PCM **240**, combined with heat transfer by the heat transfer fluid, combine to charge the thermal storage system **130** with thermal energy. This thermal energy may be retained within the thermal storage system **130** by thermally isolating thermal storage system **130** from its external environment. This is partly accomplished by insulating the external surfaces of the thermal storage system **130** with insulation **210**. However, additional components of the thermal valve are also important, including a pair of movable insulating blocks **430**. When the thermal valve is in the "closed" position (as shown in FIG. **3a**) for charging the power system **100**, these insulating blocks **430** are extended and in contact with one another to thermally isolate the thermal storage system **130** from the energy converter **150** (e.g. a TEG module). Thus, the thermal energy may be retained within the thermal storage system **130**, to continue the charging process and/or to store the thermal energy for later use. In addition to the insulating blocks **430**, the "closed" position of this example of a thermal valve may also include physically removing the energy converter **150** (e.g. TEG module) from thermal and/or physical contact with the second heat transfer plate **285**. As shown in FIG. **3a**, removal of the energy converter **150** from the second heat transfer plate **285** may be accomplished by physically attaching a movable energy converter **150** to a ram **420**. Thus, when charging the power system **100**, the ram **420** and the energy converter **150** (e.g. TEG module) may be in a retracted position, where there is not thermal/physical contact between the energy converter **150** and the relatively high temperature second heat transfer plate **285**.

In summary, when the power system **100** of FIG. **3a** is charging, heat may be added to the system and the thermal valve is in a "closed" position, such that:

1. Light **205** passes through the aperture **200** of a receiver **120**, unimpeded by insulating blocks **410**, which are in a retracted position; and
2. The energy converter **150** (e.g. a TEG module) is in a retracted position and thermally isolated from the thermal storage system **130** by insulating blocks **430** that are in an extended position and physically separate the thermal storage system **130** from the energy converter **150**.

FIG. **3b** illustrates the relationship of this example power system's elements, when discharging the thermal energy stored in the thermal storage system **130** to the energy converter **150** (e.g. TEG module) for the production of electricity. First, the insulating blocks **410** are placed in an extended position to close off the aperture **220**, which among other things, prevents heat from escaping from the receiver **120**. This minimizes heat losses, for example convective and/or radiant losses, from the thermal storage system **130** to a potentially significantly cooler outside environment (e.g. the night sky; not shown). Note: The insulating blocks **410** may also be incorporated into the design of FIG. **2** to minimize heat losses.

Discharging the energy from the power system **100** illustrated in FIG. **3b** is initiated by retracting the insulating blocks **430** to allow the ram **420** to extend the energy converter **150** (e.g. TEG module) into a position where the energy converter **150** is in physical and/or thermal contact with the second heat transfer plate **285**. In addition, retracting the insulating blocks **430** allows the cold-side surfaces of TEGs to be in thermal communication with a cooling airflow **295**, thus providing an open path from the second heat

transfer plate **285** to the airflow **295** for the transfer of non-converted thermal energy to the external environment. This in turn enables TEGs to maintain a low cold-side operating temperature,  $T_C$ , enabling the power system **100** to efficiently convert the stored thermal energy to electricity.

In summary, when the power system **100** of FIG. **3b** is discharging, the storage system is thermally insulated against heat losses and the thermal valve is in an “open” position, such that:

1. insulating blocks **410** are in an extended position and cover the aperture **200**, preventing thermal losses from the power system **100** through the aperture **200**;
2. Insulating blocks **430** are retracted, allowing physical access by the energy converter **150** to the second heat transfer plate **285**;
3. The energy converter **150** (e.g. TEG module) is extended into physical and/or thermal contact with the second heat transfer plate **285** by pushing the energy converter **150** into place using a ram **420**.

A third configuration may allow for simultaneous charging and discharging. Thermal energy enters the power system **100** in the form of light **205** while at the same time thermal energy is converted to electricity by the energy converter **150**. In this configuration:

1. Light **205** passes through the aperture **200** of a receiver **120**, unimpeded by insulating blocks **410**, which are in a retracted position; and
2. Insulating blocks **430** are retracted, allowing physical access by the energy converter **150** to the second heat transfer plate **285**;
3. The energy converter **150** (e.g. TEG module) is extended into physical and/or thermal contact with the second heat transfer plate **285** by pushing the energy converter **150** into place using a ram **420**.

The three configurations of charging, discharging, and simultaneous charging and discharging allow for fill control of the heat flow in the system, thus allowing electricity generation to be turned on and off at will.

FIGS. **4a** and **4b** illustrate another embodiment of a power system **100**. Note that the receiver is not shown in FIGS. **4a** and **4b**. However, embodiments of receivers described previously may be implemented into the power system **100** shown in FIGS. **4a** and **4b**. In the example shown in FIGS. **4a** and **4b**, a thermal valve includes a thermal cover **435**, which, when the thermal valve is in a “charging” or “closed” position as shown in FIG. **4a**, provides an insulating thermal barrier that interrupts the flow of thermal energy from the cold-side surfaces of the TEGs **270** (the energy converter **150**) to the external environment (e.g., and airflow **295**). Thus, the thermal cover **435** interrupts the path for energy transfer through the power system (see FIG. **1**). As a result, the heat exchanger **160**, the energy converter **150** (e.g. TEG module), and/or the thermal storage system **130** may eventually attain a thermal/temperature equilibrium where the hot-side temperature,  $T_H$ , of the TEGs **270** approaches and/or is equal to the cold-side temperature  $T_C$ . Referring to Equation A above, when  $T_H$  equals  $T_C$ , the TEG conversion efficiency,  $\eta$ , is zero, and none or minimal amounts of the thermal energy stored in the power system **100** may be converted to electricity. Since the thermal cover **435** retains the thermal energy (e.g. heat) in the power system **100**, the end-effect is retention of the stored thermal energy within the thermal storage system **130**.

Thus, when the thermal valve of FIG. **4a** is in the “closed” position (e.g. while charging the power system **100**), the thermal cover **435** covers, surrounds, and/or insulates the heat exchanger **160** and/or the energy converter **150** (e.g.

TEGs), isolating these elements from the surrounding environment (e.g. airflow **295**), retaining the thermal energy stored in the power system **100**. When the thermal valve of FIG. **4b** is in the “open” position (e.g. while discharging the power system **100**), the thermal cover **435** may be positioned away from the heat exchanger **160** and/or the energy converter **150**, providing a pathway for thermal energy to flow to the surrounding environment (e.g. airflow **295**). Thus, the thermal heat may be transferred to the environment, a relatively low  $T_C$  may develop at the cold-sides of an energy converter **150** using TEGs, thermal energy may be converted to electricity, and the power system **100** may discharge.

FIG. **4b** shows the arrangement of the thermal cover **435** when discharging the power system **100**. When discharging, the thermal cover **435** may be removed from the rest of the power system **100**, such that it no longer provides a barrier to heat transfer from the power system **100** to the external environment (e.g. the airflow **295**). Thus, when discharging, a relatively low temperature airflow **295** may contact the heat exchanger **160**. As a result, the heat exchanger **160** and the energy converter **150** (e.g. TEG module), which were previously at thermal equilibrium (e.g. at about  $T_H$ ) with the thermal storage system **130**, may begin to cool and drop in temperature. As a result of this cooling, the cold-side surfaces of the TEGs **270** may also cool and gradually attain a steady-state cold-side temperature,  $T_C$ . Thus, a high differential temperature may be established across the TEG module, and efficient conversion of thermal energy to electricity commences. Maintaining a low  $T_C$  and a high thermal energy to electricity conversion efficiency may be attained by increasing the heat transfer rate of the heat exchanger **160** by increasing the heat exchanger’s outside surface area by the use of a first set of fins **440**.

The thermal storage system **130** of FIGS. **4a** and **4b** utilize aspects of the systems shown in FIGS. **2**, **3a**, and **3b**. First, a plurality of heat pipes **290** is vertically positioned within the thermal storage system **130**. And, as in FIG. **2**, a first section of each heat pipe **290** is submerged and in direct physical contact with a PCM **240**, and a second portion of each heat pipe **290** extends out of the PCM **240** into an empty volume defined by a PCM/gas interface layer and a first heat transfer plate **280**. As in the previous examples, each heat pipe **290** has an internal volume containing a heat transfer fluid (not shown) But unlike the example of FIG. **2**, the heat pipes **290** of the example power system **100** shown in FIGS. **4a** and **4b** are not divided into sections by mechanical valves. Instead, similar to FIGS. **3a** and **3b**, each heat pipe **290** is a straight, uninterrupted length of pipe. However, the example of FIGS. **4a** and **4b** is unique in that a first end of each heat pipe **290** terminates in a plugged, free-floating end that is suspended within the PCM **240**. A second end of each heat pipe **290** terminates at, and is in physical and thermal communication with, the first heat transfer plate **280**.

However, the heat pipes **290** illustrated in FIGS. **4a** and **4b** function essentially in the same manner as previously described for the examples shown in FIGS. **2**, **3a**, and **3b**. Thus, when the power system **100** illustrated in FIG. **4a** is charging, heat may be transferred from the receiver (not shown) to the PCM **240**. As the PCM **240** heats up and/or melts, thermal energy may be transferred to the heat transfer fluid contained within the heat pipes **290**. Once the heat transfer fluid attains its boiling point temperature, the heat transfer fluid may begin the cycle of vaporizing and condensing, as described above, and assist with the quicker and/or more complete charging of the power system **100**. Eventually, substantially all of the PCM **240** may melt,

which in some embodiments of the power systems described herein represents a fully charged power system **100**. With the thermal cover **435** in place, the power system **100** is insulated from the external environment. Thus, additional thermal input into the power system **100** may result in further temperature rises above the target operating temperature, until all of the inside surfaces of the heat pipes **290** reach temperatures above the heat transfer fluids dew point. As a result, condensation of the heat transfer fluid within the heat pipes ceases, and eventually a steady-state mixture of saturated heat transfer fluid liquid and vapor may be attained.

Discharging the power system **100** by removal of the thermal cover **435**, allowing cooling to occur of the cold-side surfaces of the TEGs, restarts the vaporization/condensation cycle of the heat transfer fluid. As the heat exchanger **160** transfers thermal energy from the power system to the surrounding environment (e.g. airflow **295**), the heat exchanger **160** and energy converter **150** cool and their operating temperatures drop. As a result, the heat pipes **290** also cool, and some of the heat pipes' inside surface cool to the dew point temperature of the heat transfer fluid. As a result, portions of the heat transfer fluid begin to condense and heat transfer of latent heat to the first heat transfer plate **280** begins and the cycle of condensing and vaporizing the heat transfer fluid within the heat pipes **290** is resumed. This repeated vaporization and condensation of the heat transfer fluid will occur continuously, as described above, until all the surface of the heat pipes **290** attain temperatures below the boiling point temperature of heat transfer fluid. This may be when substantially all of the PCM **240** has solidified and dropped to operating temperatures below the boiling point temperature of the heat transfer fluid.

As in the embodiment of FIGS. **3a** and **3b**, the configuration shown in FIGS. **4a** and **4b** allows for simultaneous charging and discharging by removing the insulating cover while heat is input into the system. It also allows for stopping or pausing discharging before the PCM **240** is fully solidified by replacing the cover.

Referring again to FIGS. **4a** and **4b**, vaporizing zones **460** are indicated as occurring in sections of the heat pipes **290** that are submerged within the PCM **240**. Condensing zones **450** are indicated as occurring in sections of heat pipes **290** that are positioned within the empty volume of the thermal storage system **130**. However, as described above, it is to be understood that vaporization may occur in any section of heat pipe that has an operating temperature equal to or larger than the heat transfer fluid's boiling point temperature. Similarly, condensation may occur in any section of heat pipe that has an operating temperature equal to or less than the heat transfer fluid's dew point temperature. Finally, FIGS. **4a** and **4b** also illustrates an embodiment where a TEG module may be sandwiched between the first heat transfer plate **280**, and a second heat transfer plate **285**. The first heat transfer plate **280** may be in thermal communication with condensing zones **450** of the heat pipes, and also in thermal communication with the hot-side (at  $T_H$ ; see FIG. **1**) of each TEG **270**. The second heat transfer plate **285** may be a component of the heat exchanger **160**, and may be in thermal communication with the cold-side (at  $T_C$ ) of each TEG **270**. A first set of fins **440**, may be physically attached to the second heat transfer plate **285** to improve heat transfer from the heat exchanger **160** to the airflow **295**, thus maintaining a low  $T_C$ .

FIG. **5** illustrates another embodiment of a power system **100**. The thermal storage system **130** (e.g. the PCM **240**, heat pipes **290**, heat transfer fluid, etc.) may be substantially

similar to the thermal storage systems described previously. The same is true for the heat exchanger **160** (e.g. the first heat transfer plate **280**, the second heat transfer plate **285**, the energy converter **150**, the first set of fins **440** and their relationship to an airflow **295**, etc.) So, additional detailed description of these elements and features are not repeated here. While the energy converter **150** is shown to be a plurality of TEG modules **270**, it is to be understood that the TEGs could be replaced by another energy converter, such as a Stirling engine. Instead, a detailed description is provided of an alternative embodiment for a thermal valve for on-demand switching between "charging" and "discharging" states.

FIG. **5** illustrates a power system **100** having thermal valve that has a number of elements working in cooperation together. As in the previous embodiment of thermal valves describe above, the example illustrated in FIG. **5** also has at least two positions, a first "closed" position for charging the power system **100**, and a second "open" position for discharging the power system to produce electricity. The power system **100** may be switched between the positions, as needed, through the use of a heat transfer liquid. This heat transfer liquid is separate and distinct from the heat transfer fluid contained in the heat pipes **290**.

The thermal valve of FIG. **5** includes a number of elements and features, including a second heat exchanger **510** in thermal communication with the heat pipes **290**, (Note that heat exchanger **160** may also be referred to in this example as the "first" heat exchanger, and this is why the new exchangers unique to this example are referred to as "second" and "third".) This thermal communication may be established by sandwiching a third heat transfer plate **500** between the heat pipes **290** and the second heat exchanger **510**. The thermal valve may also include a third heat exchanger **520** in thermal communication with a first heat transfer plate **280** that may be in contact with the hot side of an energy converter **150**, which in this example is illustrated as a plurality of TEGs **270**. The second and third heat exchangers (**510** and **520**) may be configured to be in liquid communication with each other. The two heat exchangers may be in liquid communication due to a liquid supply line **540** linking them together (e.g. a pipe or other conduit). A pump **530** may be positioned in the liquid supply line **540**. The second and third heat exchangers (**510** and **520**) may also be in fluid communication due to the implementation of a liquid return line **550** (e.g. a pipe or other conduit).

The example of a thermal valve shown in FIG. **5** may also include a heat transfer liquid, which may be contained within the second heat exchanger **510** and the third heat exchanger **520**, within a first liquid volume **560** and second liquid volume **580**, which may be physically separated from each other by insulation **210**. These elements function together to yield a switchable thermal valve that may be switched, on-demand, between an "open" position (for discharging and/or converting thermal energy to electricity) and a "closed" position (for charging the power system **100** with thermal energy)

For example, when charging the power system **100** of FIG. **5**, the pump **530** is "off" and not circulating heat transfer liquid from the second heat exchanger **510** to the third heat exchanger **520**, through the liquid supply line **540** and liquid return line **550**. Thus, this lack of liquid flow prevents or minimizes the transfer of thermal energy from the thermal storage system **130** to the energy converter **150** because the second heat exchanger **510** remains thermally isolated from the third heat exchanger, at least partly due to separating layer of insulation **210**. The insulation **210** posi-

tioned between the second heat exchanger **510** and the third heat exchanger **520** minimizes and/or eliminates heat transfer between these two heat exchangers by blocking radiation, convective, and/or conductive losses between the second heat exchanger **510** and the third heat exchanger **520**. In addition, the liquid supply line **540** and the liquid return line **550** may both be configured such that they transfer only minimal or zero amounts of energy between the second heat exchanger **510** and the third heat exchanger **520**. For example, draining the heat transfer liquid from the second liquid volume **580** to the first liquid volume **560** may remove the heat transfer liquid from the liquid supply line **540** and the liquid return line **550** such that both lines are substantially empty. These empty pipes (or other suitable conduit), combined with an empty second liquid volume **580**, may provide a large enough resistance to heat transfer, that heat transfer from the second heat exchanger **510** to the third heat exchanger **520** is reduced or eliminated. FIG. **5** also illustrates that the second heat exchanger **510** may have an internal volume that is larger than the actual volume needed to completely drain all of the heat transfer liquid from the third heat exchanger **520** to the second heat exchanger **510** while still maintaining an empty volume **570** within the second heat exchanger **510**.

Thus, in the absence of heat transfer liquid flow between the second heat exchanger and the third heat exchanger, and energy entering the thermal storage system, is isolated from the energy converter **150** and the external environment (e.g. airflow **295**) and thermal energy is retained in the thermal storage system **130**.

When discharging the thermal energy from the power system **100** to produce electricity, the pump **530** is turned to the “on” position. When in the “on” position, the pump **530** circulates the heat transfer liquid between the second heat exchanger **510** to the third heat exchanger **520**, through the liquid supply line **540** and the liquid return line **550**. Thus, the heat transfer liquid receives thermal energy from the third heat transfer plate **500** and the temperature of the heat transfer liquid rises. The heated heat transfer liquid may then be transported/circulated by the pump **530**, through the liquid supply line **540** to the third heat exchanger **520**, where it may substantially fill the internal volume of the third heat exchanger **520**. Once filled, the heat transfer liquid may contact the first heat transfer plate **280**. This plate may initially be at a relatively cool operating temperature (e.g.  $T_c$ ), due to an outlet path for heat transfer to the external environment (e.g. airflow **295**), as described above. Thus, heat may be transferred from the relatively high temperature heat transfer liquid to the relatively low temperature first heat transfer plate **280**. At least a portion of the transferred energy may then generate electricity at the energy converter **150**, with an unconverted portion potentially ejected to an airflow **295** (e.g. heat sink). This process lowers the temperature of the heat transfer liquid, which may then be pumped and/or drains by gravity back to the second heat exchanger **510**, where it may be reheated and/or recirculated, as just described. Thus, the discharging of the power system **100** may be continuously maintained as long as sufficient thermal energy remains in the thermal energy storage system **130** (e.g. until the PCM solidifies).

Once discharging of the power system **100** is complete, or electricity generation is no longer needed, the pump **530** may be turned off stopping the circulation of heat transfer liquid between the second heat exchanger **510** and the third heat exchanger **520**. In some embodiments of the present disclosure, the pump **530** may be a positive displacement pump. In some embodiments of the present disclosure, the

pump **530** may be an electromagnetic pump and/or a mechanical pump. As in the embodiments of FIGS. **3a**, **3b**, **4a** and **4b**, the configuration in FIG. **5** allows for simultaneous charging and discharging by running the pump while energy is being input into the system. It also allows for stopping or pausing discharging before the PCM **240** is fully solidified by turning off the pump.

Note that in the embodiment of FIG. **5**, there is no phase change occurring to the heat transfer liquid; as the heat transfer liquid heats and/or cools, it remains in the liquid state. So, in this example, heat transfer from the third heat transfer plate **500** to the heat transfer liquid, and from the heat transfer liquid to the first heat transfer plate **280**, is by sensible heating and cooling of the heat transfer liquid only. Examples of the heat transfer liquid include sodium, and/or potassium. For these metal heat transfer liquids, an electromagnetic pump may be used to circulate the liquid.

FIG. **6** provides another example of a power system **100** that utilizes a second heat transfer fluid, separate and distinct from the first heat transfer fluid contained within the heat pipes **290**, where, unlike the example shown in FIG. **5**, the second heat transfer fluid undergoes a reversible liquid/vapor phase change to transfer thermal energy from the thermal storage system **130** to the energy converter **150**. The thermal storage system **130** of FIG. **6** (e.g. the PCM **240**, heat pipes **290**, heat transfer fluid, etc.) may be substantially similar to the thermal storage systems described previously. The same is true for the heat exchanger **160** (e.g. the first heat transfer plate **280**, the second heat transfer plate **285**, the energy converter **150**, the first set of fins **440** and their relationship to an airflow **295**, etc.) So, additional detailed description of these elements and features are not repeated here. Instead, a detailed description is provided of an alternative embodiment for a thermal valve for on-demand switch between “charging” and “discharging” states.

FIG. **6** illustrates a thermal valve that has a number of elements working in cooperation together, and is similar in some regards to the thermal valve described for FIG. **5**. As in the previous embodiment of thermal valves describe above, the example of FIG. **6** also has at least two positions, a first “closed” position for charging the power system **100**, and a second “open” position for discharging the power system to produce electricity. The power system **100** may be switched between the positions, as needed, through the use of a second heat transfer fluid. This second heat transfer fluid is separate and distinct from the heat transfer fluid contained in the heat pipes **290**.

The thermal valve of FIG. **6** includes a number of elements and features, including an evaporator **600** in thermal communication with heat pipes **290**. This thermal communication may be established by sandwiching a third heat transfer plate **500** between the heat pipes **290** and the evaporator **600**. The thermal valve may also include a condenser **610** in thermal communication with a first heat transfer plate **280** that is in contact with the cold-side of an energy converter **150** (as described previously). In FIG. **6**, the energy converter **150** is shown to be a plurality of TEG modules **270**, but it is to be understood that the TEGs could be replaced by another energy converter, such as a Stirling engine. The evaporator **600** and the condenser **610** are configured to be in fluid communication with each other. The evaporator **600** and the condenser **610** may be in fluid communication due to a first vapor supply line **620** and a second vapor supply line **630** linking them together (e.g. a pipe or other conduit).

The thermal valve of this embodiment, as described above, also includes the second heat transfer fluid, which is

contained within the evaporator **600** and the condenser **610**, within a first fluid volume **650** and second fluid volume **660**, respectively, which may be physically separated from each other by insulation **210**. The thermal valve of this embodiment also contains a mechanical valve **640**, positioned between the condenser **610** and the evaporator **600**. These elements function together to yield a switchable thermal valve that may be switched, on-demand, between the “open”, charging position and the “closed”, discharging position.

When discharging the power system **100** illustrated in FIG. **6**, thermal energy may be transferred from the thermal storage system **130** to the energy converter **150**, by the cyclic and repeated vaporization and condensation of the second heat transfer fluid. The mechanical valve **640** is positioned in an open position for the cycle to continue. Starting with the first fluid volume **650** of the evaporator **600**, the second heat transfer fluid may be heated by the transfer of thermal energy from the heat pipes **290**, through the third heat transfer plate **500**, and into the second heat transfer fluid contained in the evaporator **600**. If the second heat transfer fluid is initially below its boiling point temperature, it may gradually heat up and its temperature will increase. Eventually, the second heat transfer fluid may attain its boiling point temperature and begin to vaporize. The second heat transfer fluid’s vapor will pass through at least one of the first vapor supply line **620** and/or the second vapor supply line into the condenser **610**. Since in this embodiment the heat exchanger **160** is typically exposed to a cooler external environment (e.g. airflow **295**), the first heat transfer plate **280** may be at a relatively low temperature. Since the first heat transfer plate **280** is in thermal communication with at least one inside surface of the condenser **610**, the condenser **610** may also be at a relatively low operating temperature that may be below the dew point temperature of the incoming second heat transfer fluid vapor. As a result, at least a portion of the vapor may condense on the lower temperature surfaces of the condenser **610**. The condensed second heat transfer fluid may then collect in the second fluid volume **660** of the condenser and drain by gravity through the open mechanical valve **640**, and the condensate may then be returned to the first fluid volume of the evaporator **600**, where it may be reheated, revaporized, and the cycle started again. This cycle may be repeated continuously until the power system **100** is fully discharged and/or until the mechanical valve **640** is closed. FIG. **6** also illustrates that a second set of fins **660** may be included within the condensing zone of the condenser **610**, to increase the surface area available for condensing the heat transfer fluid.

Placing the mechanical valve **640** in the closed position stops the discharging process and enables charging to occur because the transfer of heat between the evaporator **600** and the condenser **610**, affected by the continuously vaporizing and condensing second heat transfer fluid, is interrupted and/or stopped. Thus, a path for heat transfer from the thermal storage system **130** to the energy converter **150** is also interrupted and the thermal energy stored in the thermal storage system is retained there. The mechanical valve **640** halts the heat transfer process by retaining the second heat transfer fluid condensate in the condenser **610**, so that it may not be vaporized in the evaporator **600**. Thus, the condensing/vaporization cycle is broken and heat transfer is stopped. Note, that the insulation **210** positioned between the evaporator **600** and condenser **610** may insure that the lower surfaces of the condenser remain cool and do not themselves attain temperatures high enough to vaporize the second heat transfer fluid. So, some insulation **210** may be necessary to

minimize conductive, convective, and/or radiant heat transfer from occurring between the evaporator **600** and the condenser **610**, when the mechanical valve **640** is in the closed position. In addition, similar to the liquid return lines described for FIG. **5**, the vapor supply lines (**620** and **630**) of FIG. **6** may be empty of vapor or liquid when the mechanical valve **640** is closed. Thus, the vapor supply lines (**620** and **630**) may likely provide a high enough resistance to heat transfer that minimal, if any, thermal “leakage” may occur from the evaporator **600** to the condenser **610**, through the vapor supply lines (**620** and **630**).

FIGS. **7a** and **7b** illustrates yet another example of a power system **100**. FIG. **7a** illustrates a “charging” state, where a thermal valve for the power system **100** is in a “closed” position, for collecting and storing thermal energy. FIG. **7b** illustrates a “discharging” state, where the thermal valve for the power system **100** is in an “open” position, for converting thermal energy to electricity. Note that the receiver is not shown in FIGS. **7a** and **7b**. However, embodiments of receivers described previously may be implemented into the power system **100** shown in FIGS. **7a** and **7b**. Also, the thermal storage system **130** of FIGS. **7a** and **7b** (e.g. the PCM **240**, heat pipes **290**, heat transfer fluid, etc.) may be substantially similar to the thermal storage systems described previously. The same is true for the heat exchanger **160** (e.g. the first heat transfer plate **280**, the second heat transfer plate **285**, the TEGs **270**, the first set of fins **440** and their relationship to an airflow **295**, etc.) So, additional detailed description of these elements and features are not repeated here. Instead, a detailed description is provided of an alternative embodiment for a thermal valve for on-demand switch between “charging” and “discharging” states.

The example of FIGS. **7a** and **7b**, as in previous examples, includes a set of heat pipes **290** positioned to be in physical contact with a PCM **240**, where the heat pipes **290** contain a heat transfer fluid. However, the power system **100** of FIGS. **7a** and **7b** includes a second set of heat pipes **730** configured to be movable between a first position where the second set of heat pipes **730** is placed in physical and/or thermal communication with a heat transfer liquid **710** contained in a vessel **700** (see FIG. **7a**), and a second position where the second set of heat pipes **730** are not in physical and/or thermal communication with the heat transfer liquid **710** (see FIG. **7b**). The vessel **700** may be configured to be in thermal communication with the first set of heat pipes **290** and may include an optional third heat transfer plate **500**. In some examples, the heat transfer liquid **710** may be a liquid that does not typically undergo a phase change during normal operating conditions. In other examples, the heat transfer liquid **710** may undergo reversible liquid-to-solid phase change.

Thus, the power system **100** of FIGS. **7a** and **7b** may charge with thermal energy as described in earlier embodiments described herein. However, the thermal energy collected in the thermal storage system **130** will remain stored there, when the thermal valve is in the “closed” position, as shown in FIG. **7a**. In this position, the heat transfer fluid **710** may come to a thermal equilibrium with the third heat transfer plate **500** and/or the thermal storage system **130**. This may also be at an equilibrium temperature that is close to or equal to the melting point temperature of the PCM **240**. If energy input into the power system **100**, for example solar energy, is continued, the temperature of the PCM **240** may continue above its melting point temperature and the operating temperature of the heat transfer liquid **710** may continue to rise as well. However, in some embodiments, once

substantially all of the mass of the PCM 240 melts, the power system 100 will be considered fully charged, and energy input into the power system 100 will be halted. Regardless, an empty volume 260 (or space) may be maintained between the heat transfer liquid 710 and the second set of heat pipes 730. This empty volume 260 may provide sufficient resistance to heat transfer between the heat transfer liquid 710 and the second set of heat pipes 730 that the energy converter 150 does not convert a significant amount of thermal energy to electricity.

FIG. 7b illustrates the thermal valve's "open" position when discharging thermal energy from the thermal storage system 130. In the "open" position the second set of heat pipes 730 are lowered to be in physical/thermal communication with the heat transfer liquid 710. Thus, a path for heat transfer may be created between the relatively high temperature PCM 240, the heat transfer liquid 710 contained in the vessel 700, the second set of heat pipes 730, and the energy converter 150. Thus, the energy converter 150 (e.g. TEGs 270) may convert the thermal energy transferred to them via this pathway to electricity. Electricity may continue to be generated as long as a sufficient differential temperature is maintained across the hot-side and cold-side of the TEGs 270, as described previously (e.g. with an outlet for non-converted thermal energy provided by the heat exchanger 160 to the external environment).

The power system 100 of FIGS. 7a and 7b may also include a seal, for example a movable bellows seal 740, to help isolate the heat transfer liquid 710 from the surrounding environment. Thus, a bellows seal 740 may help to minimize heat losses to the surrounding environment, by radiation heat loss, convective heat loss, and/or conductive heat loss, etc. Thus, a movable bellows seal 740 may be configured to expand and collapse upon itself, to move between a first position, where the bellows seal 740 is expanded to allow the second set of heat pipes 730 to move away from the heat transfer fluid 710, and a second position where the bellows seal 740 is retracted to allow the second set of heat pipes 730 to be placed in physical and/or thermal communication with the heat transfer liquid 710. Thus, a bellows seal 740 may be configured into an accordion-like structure, telescoping structure, and/or any other suitable expandable and contracting structure that enables the second set of heat pipes 730 to move reversibly between the two positions.

It should be noted, that the second set of heat pipes 730 shown in FIGS. 7a and 7b may operate in significantly the same manner as the first set of heat pipes 290. Thus, the second set of heat pipes 730 may contain a heat transfer fluid to transfer thermal energy from the heat transfer liquid 710 contained in the vessel 700 to the energy converter 150. So, the heat transfer fluid contained in the second set of heat pipes 730 may be capable of undergoing reversible phase change between a gas and a liquid. Further, the heat transfer fluid contained in the second set of heat pipes 730 may typically undergo vaporization in a first section of the second set of heat pipes 730 positioned in the heat transfer liquid 710, and condensation in a second section of the second set of heat pipes 730 positioned to be in thermal communication with the first heat transfer plate 280. However, as described above for the first set of heat pipes 290, the heat transfer fluid contained in the second set of heat pipes 730 may vaporize at any position along the vertical axis of the second set of heat pipes 730; vaporization may occur within a heat pipe at any surface that is at a temperature higher than or equal to the boiling point temperature of the heat transfer fluid. Similarly, the heat transfer fluid contained in the second set of heat pipes 730 may condense at any position along the

vertical axis of the heat second set of heat pipes 730; condensation may occur within a heat pipe at any surface that is at a temperature lower than or equal to the dew point temperature of the heat transfer fluid.

In summary, when the power system 100 of FIG. 7a is charging, the thermal storage system 130 is thermally insulated against heat losses with the external environment and the thermal valve is in an "closed" position, such that,

1. A second set of heat pipes 730 is positioned to maintain an empty volume 260 between the second set of heat pipes 730 and heat transfer liquid 710 contained in a vessel 700; and

2. A bellows seal 740 is in an extended position.

When the power system 100 of FIG. 7b is discharging, the thermal storage system 130 is thermally connected with the external environment such that thermal energy may flow from the thermal energy storage system 130, through the energy converter 150 to generate electricity, such that,

1. The second set of heat pipes 730 is positioned within a heat transfer fluid 710 to allow the transfer of heat from a first set of heat pipes 290, to the heat transfer fluid 710, from the heat transfer fluid 710 to the second set of heat pipes 730, and subsequently to the energy converter 150; and

2. The bellows seal 740 is in a retracted position.

Referring again to FIGS. 7a and 7b, a third configuration may allow for simultaneous charging and discharging. Thermal energy may be optionally entering the power system 100 (e.g. solar energy), while at the same time thermal energy may be converted to electricity by the energy converter 150, in this configuration:

1. The second set of heat pipes 730 is positioned to be in physical and/or thermal communication with the heat transfer liquid 710; and

2. The bellows seal 740 is in a retracted position.

The configuration shown in FIGS. 7a and 7b may allow for simultaneous charging and discharging by placing the second set of heat pipes 730 in thermal communication with the heat transfer liquid 710. It also allows for stopping or pausing discharging before the PCM 240 is fully solidified by removing the second set of heat pipes 730 from the heat transfer liquid 710.

FIGS. 8a and 8b illustrate an alternative configuration for the condensing zones 450 of heat pipes 290 (compare to FIG. 4). In this embodiment, a plurality of heat pipes 290 may be configured to share a single, widened condensing area, volume, and/or zone 450. A single, widened condensing zone 450 may maximize the surface area available for the heat transfer fluid contained within in the heat pipes 290, which may maximize the heat transfer rate to the TEG module (energy converter 150) and increase the electrical power output produced by the power system 100.

The following section provides modeling details of one example of a power system that utilizes some of the embodiments described herein, Referring to FIG. 9, a power system 100 is illustrated that receives light 205, in this case from the sun via one or more heliostats 910, to store thermal energy in a thermal storage system 130 that utilizes a phase change material 240. As described above, a plurality of heat pipes 290 may be positioned within the phase change material 240 to transfer energy from the phase change material 290 to a plurality of thermoelectric generators 270, when electricity generation is needed. The power system 100 may reversibly switch from energy storage to electricity generation by choosing the position of a thermal valve 140; e.g. when closed, the radiant energy received by the heat receiving surface of the thermal storage system 130 is stored in the

phase change material **240**; when opened, the radiant energy received by the heat receiving surface and/or the thermal energy stored in the phase change material **240** may be transferred by the heat pipes **290**, through the thermal valve **140** to the thermoelectric generators **270**.

An array of design criteria has been developed to theoretically demonstrate a power system similar to that shown in FIG. 9. For this theoretical example, the required electrical TEG output was assumed to be about 3 kW for about 9 hours, including 5 hours of generation from stored thermal energy. The PCM was an aluminum alloy with an operating temperature of 600° C. contained in a 0.914 m diameter tank. A TEG efficiency of about 9% and a thermal valve efficiency of about 90% were assumed, resulting in a required heat input from the PCM of about 37 kW. The thermal valve was modeled as stainless steel with a 4-layer woven mesh wick on the evaporator and the compatible working fluid is sodium (Na). The relevant design values are shown in Table 1.

TABLE 1

Parameters used to calculate thermal valve design	
Quantity	Value
Vessel Material	¼" Stainless Steel 304
Working Fluid	Sodium
Operating Temperature	600° C.
Heat Transfer	37 kW
Evap/Cond Diameter	0.914 m
Na, Mass Flow Rate	0.00873 kg/s
Na, Heat of Vaporization	4236 KJ/kg
Na, Liquid Density	805.4 kg/m <sup>3</sup>
Na, Vapor Density	0.013 kg/m <sup>3</sup>

The thermal valve **140** example modeled here, similar to that shown in FIG. 6, is based on a gravity-assisted thermosiphon. As illustrated in FIG. 10a, an evaporator **600** may be constructed as a horizontal surface at the bottom of a thermal valve **140**, with a condenser **610** configured as a horizontal surface at the top of a thermal storage system (not shown)

The top of the thermal storage system (e.g. a PCM tank; not shown in FIGS. 10a and 10b) may contact the outer surface of the evaporator **600** to heat the working fluid contained within the thermal valve **140**. This working fluid may then be vaporized and removed from the evaporator **600**, such that the vapor flows (represented by the upward dashed arrows) through one or more vapor tubes **1100** by a pressure gradient, such that the vapor is transferred to the top inner condenser surface of the condenser **610** where the working fluid condenses. There, the working fluid's latent heat may be transferred through an outer wall of the condenser **610** to a heat sink (not shown), for example, to a TEG array (not shown). The working fluid condensate may then flow down a condensate funnel **1200**, into a liquid return tube **1300** (e.g. liquid return line), and through an open mechanical valve **640** (e.g. a mechanical ball valve). From there, the working fluid condensate may flow over a diverter cone **1000** where it then returns to the evaporator where a wick (not shown) may pull and spread the liquid working fluid across the evaporator surface. The liquid working fluid may then absorb additional heat from the PCM through the evaporator wall, resulting in the re-vaporization of the working fluid to restart the heat pipe/thermosiphon cycle.

Referring to FIG. 10b, in the "off" state, the mechanical valve **640** is closed. Any liquid working fluid on the lower

hot surface of the evaporator **600** evaporates, flows up the vapor tubes **1100**, to condense in the condenser **610**. The working fluid condensate may then flow down to collect in the funnel **1200**, with access to the evaporator **600** blocked by the closed mechanical valve **640**. As a result, the evaporator **600** may dry out, as substantially all of the working fluid may evaporate to condense and collect in the condenser. This in turn halts the heat pipe cycle. In this way, the flow of heat to the TEGs may be modulated as electrical demand requires.

The sections below present a detailed analysis of a pressure model and a thermal resistance model that investigate some embodiments of the present disclosure. A heat pipe pressure model was used to predict the operability of the power system summarized in Table 1 above. A heat pipe may function if the capillary pumping pressure exceeds the sum of all pressure drops and gains in the system. If the sum of the pressure losses/gains exceed the capillary pumping pressure, the evaporator may "dry-out", overheat, and may lose the ability to transfer a practical quantity of heat. This relation is expressed mathematically as,

$$\Delta P_{cap,max} \geq \Delta P_1 + \Delta P_v + \Delta P_e + \Delta P_c + \Delta P_g \tag{1}$$

where  $\Delta P_{cap,max}$  is the maximum capillary pumping pressure of the wicking structure in the evaporator,  $\Delta P_1$  is the pressure loss due to viscous energy losses in the liquid flow,  $\Delta P_v$  is the pressure loss due to viscous energy losses in the vapor flow,  $\Delta P_e$  and  $\Delta P_c$  are the evaporation and condensation phase change pressure drops, and  $\Delta P_g$  is the pressure loss or gain due to gravitational body forces.

The liquid returning to the evaporator from the liquid condensate tube should optimally spread evenly over the wicking surface with a low pressure loss due to viscous effects. A "diverter cone" was implemented in the design to minimize the distance that the liquid must travel to cover the entire evaporator surface. When dropping from the edges of the diverter cone, the liquid spreads radially inward and outward over the evaporator surface. The radial differential Darcy relation was used to calculate the viscous liquid pressure loss through the porous media of the multi-layer woven wicking structure,

$$v = \frac{-\kappa}{\mu_l} \frac{dp}{dr} \tag{2}$$

where v is the discharge volume per unit area,  $\kappa$  is the permeability of the porous wick,  $\mu_l$  is the liquid dynamic viscosity, and  $dp/dr$  is the change in pressure (p) over a radial distance (r). Replacing the discharge volume per unit area with the volume flow rate ( $\dot{V}$ ) and the cross sectional area ( $2\pi rh$ ) of the flow over a disc gives,

$$\frac{\dot{V}}{2\pi rh} = \frac{-\kappa}{\mu_l} \frac{dp}{dr} \tag{3}$$

where r is the radius and h is the height of the flow area. To attain the change in pressure as a fluid moves from one radius ( $r_1$ ) to another ( $r_2$ ), the expression is rearranged and integrated.

$$\int_{r_1}^{r_2} \frac{dr}{r} = \int_{p_1}^{p_2} \frac{-2\pi h \kappa}{\mu_l \dot{V}} dp \tag{4}$$

That integration leads to the following expression,

$$\ln\left(\frac{r_2}{r_1}\right) = \frac{-2\pi hk}{\mu_l \dot{V}} (p_2 - p_1) \quad (5)$$

Isolating the pressure drop from  $r_1$  to  $r_2$  gives,

$$(p_2 - p_1) = \frac{-\mu_l \dot{V}}{2\pi hk} \ln\left(\frac{r_2}{r_1}\right) \quad (6)$$

Adding that the volume flow rate is related to the heat flow ( $q$ ), the heat of vaporization ( $H_v$ ), and the density ( $\rho$ ), the following final expression represents the pressure loss of fluid flowing radially in a 2-D porous medium of a given porosity from  $r_1$  to  $r_2$ .

$$\Delta p_l = \frac{-\mu_l q}{2\pi hk \rho H_v} \ln\left(\frac{r_2}{r_1}\right) \quad (7)$$

This viscous liquid pressure loss through the wick was then compared to the capillary pumping pressure ( $\Delta P_{cap,max}$ ) developed in the wick pores, given by the Young-Laplace relation

$$\Delta P_{cap,max} = \frac{2\sigma}{r_{eff}} \quad (8)$$

where  $\sigma$  is the liquid surface tension and  $r_{eff}$  is the effective capillary radius of the wick pores.

Very small wick sizes promote higher capillary pumping pressure and may create many sites for vapor nucleation, while at the same time, increasing the viscous liquid pressure losses. Very large wick sizes provide little or no capillary pumping pressure and few sites for nucleation, though the losses due to viscous effects may be small. To find a reasonable balance between the two extreme effects, the viscous liquid pressure losses and the corresponding capillary pressures for an array of mesh sizes was plotted and is shown in FIG. 11.

FIG. 11 illustrates that the viscous pressure loss balances the capillary pumping pressure with a value of 2000 Pa with woven mesh sizes around 100 #/inch. Using a larger mesh size (smaller #/inch) would decrease the number of nucleation sites, resulting in diminished evaporative heat transfer rate while using a smaller mesh size would result in prohibitively high liquid viscous pressure loss. For the current design, it was concluded that four-layer 100 #/inch would provide a satisfactory balance between viscous losses and vapor nucleation.

Viscous vapor pressure loss occurs when the vapor flows from the evaporator to the condenser through the vapor passageway. In the thermal valve design presented here, the vapor travels through three vertical vapor tubes. Given the design heat flow of 37 kW and the heat of vaporization of Na, the required vapor volume flow rate is 0.672 m<sup>3</sup>/s. The vapor velocity of this device is designed to the incompressible regime and with a Mach number < 0.2. The speed of sound in the Na vapor at 600° C. is calculated with the Newton-Laplace relation,

$$v_{sound} = \sqrt{\frac{\gamma RT}{M}} \quad (9)$$

where  $\gamma$  is the adiabatic index which is 5/3 for the monatomic sodium vapor. R is the molar gas constant (8.315 J/mol-K), T is the absolute temperature, and M is the molar mass of the vapor. Using the design parameters of the thermal valve, the velocity of sound in the sodium vapor was found to be about 726 m/s, resulting in a vapor tube velocity of 145 m/s at Mach 0.2. The vapor tube diameter for this design was then specified to be about 4.43 cm.

Now, knowing the vapor tube diameter, the vapor viscous pressure loss was then determined. First, the friction Reynold's number was calculated using the relation,

$$(f_v Re_v) = 0.038 \left[ \frac{2(r_{h,v})q}{A_v \mu_v H_v} \right]^{3/4} \quad (10)$$

where  $r_{h,v}$  is the vapor tube hydraulic radius,  $A_v$  is the vapor area, and  $\mu_v$  is the vapor viscosity. This was then used to calculate the pressure drop using the following relation,

$$\Delta P_v = \left[ \frac{C(f_v Re_v) \mu_v}{2r_{h,v}^2 A_v \rho_v H_v} \right] L_{eff} q \quad (11)$$

where C is 1.00 for incompressible flow and  $L_{eff}$  is the effective length of the vapor flow. Using the given system design parameters, the resulting vapor viscous pressure drop is 46.0 Pa.

Besides the major viscous losses due to vapor and liquid flow, there may be other pressure losses and gains in a thermal valve system. The hydrostatic pressure gain of the thermal valve is due to the gravity return of the condensate from the condenser back down to the evaporator. This gain is simply calculated from the Bernoulli relation,

$$\Delta P_g = \rho_l g h \quad (12)$$

where g is the acceleration due to gravity and h is the height from the evaporator surface to the condenser surface. With the 0.899 m vertical height of the thermal valve, the resulting hydrostatic pressure gain is about 6724 Pa.

The final pressure terms,  $\Delta P_e$  and  $\Delta P_c$ , develop across the condensation and evaporation phase change boundaries. These values are typically many orders of magnitude smaller than all other pressure terms for high-temperature heat pipes and were neglected for this analysis. Table 2 shows the magnitude of each of the contributing pressure terms for the 3 kW thermal valve device.

TABLE 2

Contributing pressure terms in the STEALS thermal valve and their calculated values.		
Pressure	Symbol	Value (Pa)
Capillary Pumping	$\Delta P_{cap,max}$	+2394
Viscous Liquid	$\Delta P_l$	-2031
Viscous Vapor	$\Delta P_v$	-46.0
Phase Change	$\Delta P_e, \Delta P_c$	~0
Hydrostatic	$\Delta P_g$	+6724
Surplus	$\Delta P_{surplus}$	+7041

These values are plotted along the effective length of thermal valve and are shown in FIG. 12.

Starting at the liquid/vapor surface of the evaporator, the vapor flows up through the vapor tubes where it then releases latent heat and condenses along the length of the condenser at 140 cm. That condensate then drops back down to the evaporator gaining a large hydrostatic pressure. The liquid then flows across the evaporator wick, losing viscous liquid pressure along the way. This liquid was pulled along the wick by the positive capillary pumping pressure provided by the wick capillary pores. Summing the calculated pressure drops results in a surplus of 7041 Pa around the system, indicating that the example device will function as intended.

A thermal resistance model was developed to predict the performance characteristics of the thermal valve in both the "on" state and the "off" state. A diagram of the contributing individual thermal resistances in a network is shown in FIG. 13. From the PCM, the heat flows through the evaporator wall, the saturated wick, and the liquid-vapor interface. From there, heat flows by pressure-driven convection with the Na vapor in the "on" state, by conduction through the vapor tube walls, and by radiation in the "off" state. At the condenser, the heat flows through the vapor-liquid interface, the condensate film, and through the condenser wall, where the heat is transferred through the TEG and finally rejected through a forced or natural convection heat sink.

Fourier's law was used to calculate the thermal resistance due to conduction heat transfer,

$$R = \frac{\Delta x}{kA} \quad (13)$$

where  $\Delta x$  is the material thickness,  $k$  is the thermal conductivity, and  $A$  is the cross sectional area. This relation was used to calculate the thermal resistance of the evaporator and condenser walls ( $R_{evap, wall}$ ,  $R_{cond, wall}$ ), the saturated wick ( $R_{evap, wick}$ ), the axial heat transfer through the vessel walls ( $R_{wall, axial}$ ), the axial vapor resistance in the "off" state ( $R_{vapor}$ ), and the condensate film on the condenser ( $R_{condensate}$ ).

The effective thermal conductivity of the sodium saturated multi-layer woven mesh wick was determined with the following relation,

$$k_{eff, mesh} = \frac{k_l[(k_l + k_s) - (1 - \varphi)(k_l - k_s)]}{[(k_l + k_s) + (1 - \varphi)(k_l - k_s)]} \quad (14)$$

where  $k_l$  is the liquid thermal resistance (sodium),  $k_s$  is the solid thermal resistance (stainless steel), and  $\varphi$  is the porosity of the wick. The thermal resistance of the flowing vapor in the "on" state was calculated with the following relation,

$$R_{v,a} = \frac{T_v(P_{v,e} - P_{v,c})}{\rho_v H_v q} \quad (15)$$

where  $T_v$  is the vapor temperature,  $P_{v,e}$  and  $P_{v,c}$  are the vapor pressures at the evaporator and condenser respectively. In the "off" state, the radiation heat transfer from the hot evaporator to the cooler condenser through the vapor tubes was calculated from the standard radiation relation,

$$Q_{rad} = \sigma N_{tubes} \frac{T_{evap}^4 - T_{cond}^4}{R_{rad}} \quad (16)$$

where  $\sigma$  is the Stefan-Boltzmann constant,  $N_{tubes}$  is the number of vapor tubes,  $T_{evap}$  and  $T_{cond}$  are the evaporator and condenser temperatures, and  $R_{rad}$  is the equivalent resistance of the radiation network. The radiation network of this power system consists of radiation directly from the evaporator to the condenser in parallel with the radiation from evaporator to the tube and then from the tube to the condenser and is represented by the following relation,

$$R_{rad} = \frac{2}{A(F_{ec} + 1)} \quad (17)$$

where  $A$  is the cross-sectional area of the vapor tube and  $F_{ec}$  is the view factor from one circular area to another parallel circular area. This is given by,

$$F_{ec} = \frac{S - \sqrt{S^2 - 4}}{2} \quad (18)$$

where  $S$  is a geometric factor relating the circle radius to the distance between them.

The calculated values for each individual thermal resistance is shown in Table 3 below.

TABLE 3

Thermal resistance values of the thermal valve in both the "on" and "off" states.			
Resistance	Symbol	"On" Value (K/W)	"Off" Value (K/W)
Evaporator Wall	$R_{evap, wall}$	0.000496	0.000496
Evaporator Wick	$R_{evap, wick}$	$1.98 \times 10^{-5}$	N/A
Liquid-Vapor Phase	$R_{liq-vap}$	$1.27 \times 10^{-9}$	N/A
Vapor Axial Walls	$R_{vapor}$	$59.1 \times 10^{-6}$	13933
Radiation	$R_{wall, axial}$	72.8	72.8
Vapor-Liquid Phase	$R_{rad}$	N/A	7.37
Condensate	$R_{vap-liq}$	$1.27 \times 10^{-9}$	N/A
Condenser Wall	$R_{condensate}$	$4.26 \times 10^{-8}$	N/A
Total	$R_{cond, wall}$	0.000496	0.000496
		0.00103	5.65

The thermal resistance analysis shows a 5500x change in total resistance from the "on" state to the "off" state. A graphical representation of the degree of thermal resistance and heat flow contributions is shown in FIG. 14.

It is evident that the largest contributors to the "on" thermal resistance are the evaporator and condenser walls at 48% each. The magnitude of these can be further decreased by applying thinner and/or more thermally conductive materials. The largest heat flow paths in the "off" state are the parallel paths of radiation through the vapor tubes (~77%) and solid conduction through the vessel walls (~23%). Radiation heat loss may be minimized with internal radiation shields above and/or below the vapor tubes or simply by bending an arc shape into the vapor tubes to minimize the line-of-sight from the evaporator to the condenser. Additionally, the axial heat loss through the walls may be reduced by applying thinner and/or less thermally conductive mate-

rials. Both of these diagrams indicate where optimization may improve the thermal performance characteristics of the device.

The pressure model was developed for the model power system. A summation of all pressures in the system concluded that it will function with a pressure surplus of 7 kPa, largely due to the hydrostatic pressure gain. Additionally, a thermal resistance network model was analyzed to determine the thermal performance of the device in the “on” and “off” states. The model predicts a 5500x difference between the “on” and “off” state thermal resistances.

As used herein, the term to be in “thermal communication” refers to the ability of a first object to transfer energy, e.g. heat, to a second object. This transfer of energy may occur by conduction, convection, radiation, and/or any other suitable means of heat transfer. As used herein, the term “substantially” refers to a complete whole or near complete whole of something, or the complete absence or near complete absence of something. This term may be used to recognize that in certain engineering circumstances obtaining 100% of something, e.g. heat transfer, or eliminating 100% of something, may not be physically possible. So, in some instances, “substantially” may refer to from 99% to 100%, from 98% to 100, from 97% to 100%, or from 90% to 100% of the metric being referred to. In some instances, “substantially” may refer to from 0% to 1%, from 0% to 2%, from 0% to 3%, or from 0% to 10% of the metric being referred to.

FIG. 14 illustrates a method 1400 for receiving thermal energy from an energy source, storing the thermal energy received, and converting the thermal energy to electricity. In some embodiments of the present disclosure, the method 1400 may begin by receiving thermal energy 1410 from an energy source (e.g. solar, geothermal, industrial). The receiving of the thermal energy 1410 may be accomplished using a suitable receiver, as described above. The method 1400 may then include the transferring of the thermal energy 1420 to a phase change material (PCM), where the PCM may be stored in an appropriately sized container, as described above. The thermal energy transferred to the PCM may then be stored there for a period of time or immediately transferred to the next step of the method 1400. For example, the method 1400 may include storing of the thermal energy 1430 in the PCM for a desired amount of time, before delivering the thermal energy 1440 stored in the PCM to a heat transfer fluid, as described above. Alternatively, the method 1400 may immediately transfer the thermal energy transferred to the PCM by delivering the thermal energy 1440 to the heat transfer fluid. The method 1400 may also include transferring the thermal energy to an energy converter 1450 and converting the thermal energy to electricity 1460, as described above.

## EXAMPLES

### Example 1

A system comprising: a container comprising an internal volume at least partially defined by a wall having an external surface; a moveable surface having a first position and a second position; and a heat transfer fluid positioned within the internal volume, wherein: when in the first position, the moveable surface is substantially thermally isolated from the external surface such that substantially no heat is transferred from the heat transfer fluid, through the external surface, to the moveable surface, and when in the second position, the moveable surface is in thermal communication with the

external surface such that heat is transferred from the heat transfer fluid, through the external surface, to the moveable surface.

### Example 2

The system of Example 1, further comprising: a ram having a retracted position and an extended position, wherein: the moveable surface is physically attached to the ram, when in the retracted position, the ram places the moveable surface in its first position, and when in the extended position, the ram places the moveable surface in its second position.

### Example 3

A system comprising: a container comprising an internal volume at least partially defined by a wall having an external surface; a moveable surface having a first position and a second position; a first heat transfer fluid positioned within the internal volume; and a second heat transfer fluid positioned external to the internal volume, wherein: when in the first position, the moveable surface is positioned between the external surface and the second heat transfer fluid such that the first heat transfer fluid is substantially thermally isolated from the second heat transfer fluid, and when in the second position, the moveable surface is positioned such that the first heat transfer fluid is in thermal communication with the second heat transfer fluid such that heat is transferred from the first heat transfer fluid to the second heat transfer fluid, through the external surface.

### Example 4

A system comprising: a first container comprising a first internal volume at least partially defined by a first wall; a first heat transfer fluid positioned within the first internal volume; a second container comprising a second internal volume at least partially defined by a second wall; a second heat transfer fluid positioned within the second internal volume; a fluid conduit that fluidly connects the first internal volume with the second internal volume; a fluid transport means positioned within the fluid conduit and having a first position and a second position; and an energy converter configured to be in thermal communication with the second wall, wherein: when in the first position, the second heat transfer fluid is substantially thermally isolated from the energy converter, when in the second position, heat is transferred from the first heat transfer fluid through the first wall to the second heat transfer fluid, when in the second position, a portion of the heat transferred is delivered from the second heat transfer fluid through the second wall to the energy converter by cycling, using the fluid transport means, the second heat transfer fluid from the first container to the second container, and from the second container back to the first container, and the energy converter converts the portion of the heat transferred to electricity.

### Example 5

The system of Example 4, wherein: the second heat transfer fluid is a liquid, the fluid transport means consists of a pump, when in the first position, the pump is off, when in the second position, the pump is on such that the pump transports the second heat transfer fluid from the first

container to the second container, and the heat transfer fluid is transported from the second container to the first container by gravity.

#### Example 6

The system of Example 4, further comprising: a mechanical valve; and a vapor conduit that fluidly connects the first internal volume with the second internal volume, wherein: the second heat transfer fluid is in at least one of a liquid state or a vapor state, when in the first position, the mechanical valve is closed such that substantially all of the second heat transfer fluid is accumulated in the second internal volume in the liquid state, when in the second position, the mechanical valve is open such that the second heat transfer fluid is converted from the liquid state to the vapor state, the second heat transfer fluid in the vapor state is transported from the first container through the vapor conduit to the second container, the second heat transfer fluid in the vapor state condenses on the second wall to form the second heat transfer fluid in the liquid state, and the second heat transfer fluid in the liquid state returns through the open valve to the first container, and the fluid transport means consists of a vacuum created by the condensing second heat transfer fluid and gravity.

#### Example 7

A system comprising: a first container comprising a first internal volume at least partially defined by a first wall; a first heat transfer fluid positioned within the first internal volume; a second container comprising a second internal volume at least partially defined by a second wall in thermal communication with the first wall; a second heat transfer fluid positioned within the second internal volume; a third container comprising a third internal volume at least partially defined by a third wall and a fourth wall; a third heat transfer fluid positioned within the third internal volume, and an energy converter configured to be in thermal communication with the fourth wall, wherein: the third container has a first position and a second position, when in the first position, the third container is positioned to be substantially thermally isolated from the second heat transfer fluid such that substantially no heat is transferred to the energy converter, when in the second position, the third container is positioned in thermal communication with the second heat transfer fluid such that heat is delivered from the first heat transfer fluid to the second heat transfer fluid through the first wall and the second wall, at least a first portion of the heat delivered is transferred from the second heat transfer fluid to the third heat transfer fluid through the third wall, and at least a second portion of the heat delivered is transferred from the third heat transfer fluid to the energy converter through the fourth wall, such that the energy converter converts the second portion of the heat to electricity.

The foregoing discussion and examples have been presented for purposes of illustration and description. The foregoing is not intended to limit the aspects, embodiments, or configurations to the form or forms disclosed herein. In the foregoing Detailed Description for example, various features of the aspects, embodiments, or configurations are grouped together in one or more embodiments, configurations, or aspects for the purpose of streamlining the disclosure. The features of the aspects, embodiments, or configurations, may be combined in alternate aspects, embodiments, or configurations other than those discussed above. This

method of disclosure is not to be interpreted as reflecting an intention that the aspects, embodiments, or configurations require more features than are expressly recited in each claim. Rather, as the following claims reflect, inventive aspects lie in less than all features of a single foregoing disclosed embodiment, configuration, or aspect. Thus, the following claims are hereby incorporated into this Detailed Description, with each claim standing on its own as a separate aspect, embodiment, or configuration,

What is claimed is:

#### 1. A system comprising:

- a thermal valve having a first position and a second position; a heat transfer fluid;
- a receiver configured to receive thermal energy; a phase change material (PCM);
- a heat pipe comprising a first internal volume at least partially defined by a first wall and a second wall; and

an energy converter, wherein:

the heat transfer fluid is positioned within the first internal volume, the PCM is in thermal communication with the heat transfer fluid through the first wall, the energy converter is configured to be in thermal communication with the heat transfer

fluid through the second wall,

when in the first position, the thermal valve prevents the transfer of the thermal energy from the PCM to the energy converter, and enables the transfer of the thermal energy from the receiver to the PCM, and when in the second position, the thermal valve enables the transfer of the thermal energy from the PCM to the heat transfer fluid and the energy converter, such that the energy converter converts at least a portion of the thermal energy to electricity.

#### 2. The system of claim 1, wherein

the thermal energy comprises at least one of solar energy, geothermal energy, or energy from industrial sources.

#### 3. The system of claim 2, wherein:

when in the first position, the thermal valve thermally and physically separates the second wall from the energy converter, and

when in the second position, the energy converter is in physical contact with the second wall.

#### 4. The system of claim 1, wherein the heat pipe is in the form of at least one of a vertically oriented cylinder or vertically oriented duct.

#### 5. The system of claim 4, further comprising a wicking structure positioned within the first internal volume.

#### 6. The system of claim 1, wherein the energy converter comprises at least one of a thermoelectric generator or a heat cycle.

#### 7. The system of claim 6, wherein the heat cycle comprises at least one of a Stirling Cycle, a Rankine Cycle, or a Brayton Cycle.

#### 8. The system of claim 1, further comprising:

a container having a second internal volume, wherein: the PCM is positioned within the second internal volume, and the heat pipe is at least partially immersed in the PCM.

#### 9. The system of claim 1, wherein the heat transfer fluid has a boiling point between 500° C. and 800° C.

#### 10. The system of claim 9, wherein the boiling point is at a pressure less than 1 atmosphere.

#### 11. The system of claim 1, wherein the heat transfer fluid comprises at least one of sodium or a sodium-potassium eutectic material.

12. The system of claim 11, wherein the sodium-potassium eutectic material comprises NaK.

13. The system of claim 1, wherein the PCM undergoes a reversible liquid-to-solid phase transition at a temperature between 500° C. and 800° C.

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14. The system of claim 13, wherein the PCM comprises at least one of aluminum or an aluminum alloy.

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