

88PC-88935-QTR-8

**INHIBITION OF RETROGRESSIVE REACTIONS
IN COAL/PETROLEUM CO-PROCESSING**

QUARTERLY TECHNICAL PROGRESS REPORT
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OBJECTIVE

The overall objective of this project is to develop a fundamental understanding of the reactions occurring at the onset of coke formation during the co-processing of coals with petroleum residua. The specific objectives include examination of chemical components, or groups of components, in coals and petroleum feedstocks to quantify and rank the effects of these components in retarding or enhancement of coke formation. The work involves bench scale reactions in microautoclaves, supplemented by studies of the carbonaceous residues by such techniques as diffuse reflectance Fourier transform infrared spectroscopy and ^{13}C nuclear magnetic resonance spectrometry.

During this reporting period microautoclave testing of mixtures of model compounds and coal was concluded. In addition mixtures of coals and petroleum feedstocks were reacted under the same reaction conditions as used for the model compounds experiments. The petroleum resids were also independently tested in absence of coal. For a set of coal/resid feedstock pairs tests were performed in both horizontal and vertical microautoclaves in order to compare the mixing properties of these two different designs.

SUMMARY

The focus of the work during this reporting period was the solvation and dispersion relationship involving the reactions of coals with five model compounds: eicosane, 1-phenyldodecane, 1,4-diisopropylbenzene, durene, and pyrene and two petroleum vacuum resids, namely FHC-571 and FHC-470. Reactions were performed under a hydrogen atmosphere and were compared to the results of the reactions when nitrogen was used. Coal conversions for the model compound reactions and the co-processing reactions were compared. The influence of temperature, gas atmosphere , and feedstock on the percent of coal conversion were examined. The influence of mass transfer was examined using vertical and horizontal microautoclaves for a selected number of experiments. The solid residue was analyzed by ^{13}C NMR and these spectra were compared to the baseline ^{13}C NMR spectra of the coal.

TASK 1: SELECTION OF FEEDSTOCK

As reported earlier this Task is essentially finished. Some additional resid samples will be acquired at a later date when the process chemistry now being developed will allow us to specify in advance a "good" and "poor" resid.

TASK 2: IDENTIFICATION OF SOLVATION AND DISPERSION REALTIONSIPS

Model Compound Reactions

During this reporting period, the five project coals were reacted with the five model compounds under a hydrogen atmosphere (Appendix 1). The results of the reactions under a nitrogen atmosphere were previously reported [1]. The reaction temperatures were 350°, 400°, and 450° C, and the starting pressure was 3.5 MPa. Coal conversion is defined on the basis of yield of THF-insolubles as:

$$\text{Conv\%} = \left[1 - \frac{\text{THFinsoluble}}{\text{Wt.coal (daf)}} \right] \times 100$$

Gas atmosphere effect

There does not seem to be a consistent influence of the gas atmosphere on coal conversion in the model compound reactions. Comparisons of coal conversions under a nitrogen and hydrogen atmosphere at a given temperature are shown in Figures 1-15. Under the given conditions of these tests, namely 3.5 MPa of nitrogen or hydrogen, the differences in degree of coal conversions are not significant. It is generally expected that the conversions would increase in the presence of hydrogen gas, but under the given reaction conditions the effect of the chemical nature of the coal and the model compound seem to override the effects of the gas atmosphere. At the lowest reaction temperature of 350° C the coal conversions are generally higher when hydrogen gas is present for all model compounds except pyrene. In the reactions of pyrene and coal comparably high coal conversions were achieved under a nitrogen atmosphere and in some cases even higher than under a hydrogen atmosphere. Once again, as mentioned in the earlier report [1], pyrene exhibits significantly different behavior than any of the other four model compounds.

Temperature effect

The reaction temperature has a different effect on the conversion of the five coals. Figures 16-20 show the coal conversion with different feedstock and reaction temperatures with hydrogen gas overpressure, and Figures 21-25 show the respective coal conversions under a nitrogen atmosphere. For the two lower rank coals used in this project , subbituminous B (PSOC 1488) and hvC bituminous (PSOC 1498) the coal conversion increases with increasing temperature of reaction. The exceptions are reactions with pyrene when the maximum coal conversions are achieved at 400° C. For the three remaining project coals (hvB and hvA bituminous) the highest coal conversions are obtained at 400°C. This pattern is observed when nitrogen or hydrogen overpressure is used. The reason for this behavior probably is that the higher rank project coals all have their temperature of maximum fluidity above 400° C while the two lower rank coals have FSI's of 0 and 0.5 respectively.

Reactions with Petroleum Resids

Thermal stability tests on the two petroleum resids were completed. The yield of THF-insolubles was observed in reactions under a nitrogen atmosphere and under a hydrogen atmosphere. The results in Appendix 2. show that neither of the vacuum feed resids, FHC-571 and FHC-470 produced a significant amount of insolubles at 350° or 400° reaction temperatures. The yield of insolubles increases at 450° C. In the case of FHC-571 the maximum yield insoluble is 3% of the total weight of resid. For the sample FHC-470 the yield insoluble is greater, around 15% of the total weight of the resid. The gas atmosphere does not seem to influence the production cf insolubles from these two petroleum resid feedstock.

The two resids were reacted with the five project coals under the same reaction conditions as the model compound reactions. A nominal charge of 2.5g of coal and approximately 5g of resid were reacted in microautoclaves. Due to the high viscosity of the petroleum resids, the loadings varied anywhere from 4.5 to 6 g. Reactions were conducted using nitrogen and hydrogen overpressure of 3.5MPa at the beginning of the reaction. The results in Appendix 2 show that the amount of insolubles formed is the smallest at reaction temperature 400° C. On the other hand, at temperature 450° C the yield of insolubles dramatically increases.

Comparing these results to the previous thermal stability tests of the coal alone and resid alone, it is obvious that none of the project coals or petroleum resids produced this high yield of insolubles. The interactions between the coal particles and petroleum resids at the highest reaction temperature seem to favour the retrogressive reactions and the formation of insoluble matter. The Figures 16-25 show that coal conversion is steadily negative at reaction temperature 450° C in the presence of petroleum resids. On the other hand, the coal conversions in the reactions with petroleum resids at 400° C are in the range of those conversion achieved in the presence of pyrene. It was previously noted that of all the model compounds tested in this project pyrene acted most favorably in terms of minimizing the production of THF-insolubles. The results indicate that petroleum resids are as good solvents for coal particles as pyrene for reaction temperatures less than 450° C.

For most of the coals used in reactions with petroleum resids, higher conversions were obtained in the presence of hydrogen. The exception is the high volatile A, PSOC 1448 coal when reactions with nitrogen overpressure resulted in higher coal conversion.

Microreactor Design Comparison Reactions:

A selected number of coal-model compound pairs were reacted under same reaction conditions (pressure and temperature) in a vertical tubing bomb reactor normally used in this project and a horizontal one of the same volume. The reason for this is to test the mixing properties and mass transfer effects of these two different designs, and to evaluate the effect of the microreactor design on the yield of insoluble matter hence, coal conversion. For this purpose one coal and one reaction temperature were chosen and were reacted with eicosane, diisopropylbenzene and, pyrene in a nitrogen and hydrogen atmosphere. The table with the collected data for these experiments is in Appendix 1. The yield of insolubles when horizontal microreactors are used are lower by 2-4% compared to the experiments with the vertical design. This result seems to be in agreement with the results reported by Rhee et al [2]. that the horizontal oriented microreactors have advantage over the vertical oriented microreactors in terms of mixing properties in the absence of agitator balls. For the scope of this project though, these differences are not that significant and under the reaction conditions used here the design of the microreactor does not seem to have a great effect.

Characterization of Solids Products

A number of solid residue were analyzed by ^{13}C NMR. The instrument used was a Chemagnetics MS-100. Appendix 3. contains the spectra of the insoluble residue of thermal reactions of PSOC1488 under nitrogen and hydrogen at various temperatures and a spectra of a residue of unreacted coal after extraction with THF. Most obvious is the expected decrease in the aliphatic region and the accompanying increase in the aromatic region. This change is more apparent when the reaction temperatures is increased from 400° C to 450° C and less when the increase is from 350° C to 400° C. Similar observations were previously reported [1] from the information gained by comparing the DRIFT spectra.

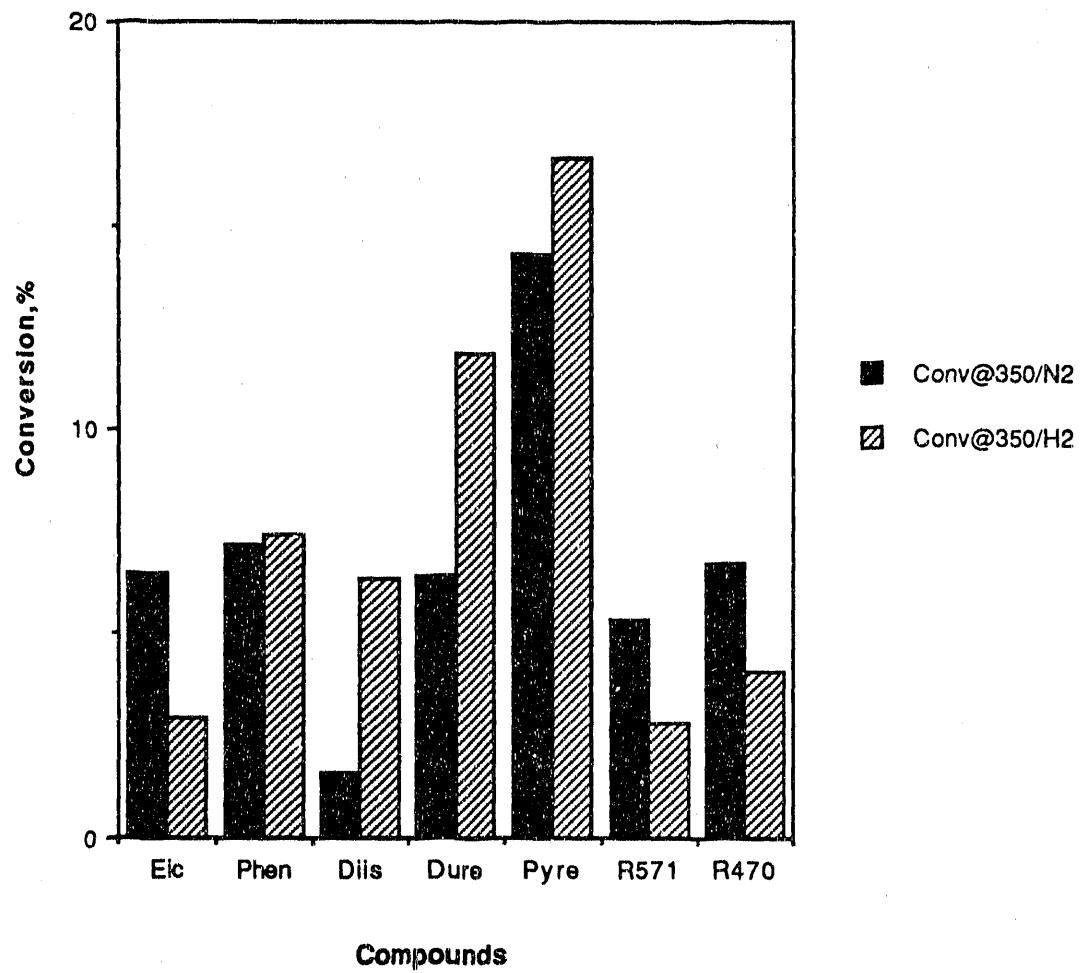


Figure 1. Conversion for PSOC1448 under N_2 and H_2 at 350°C

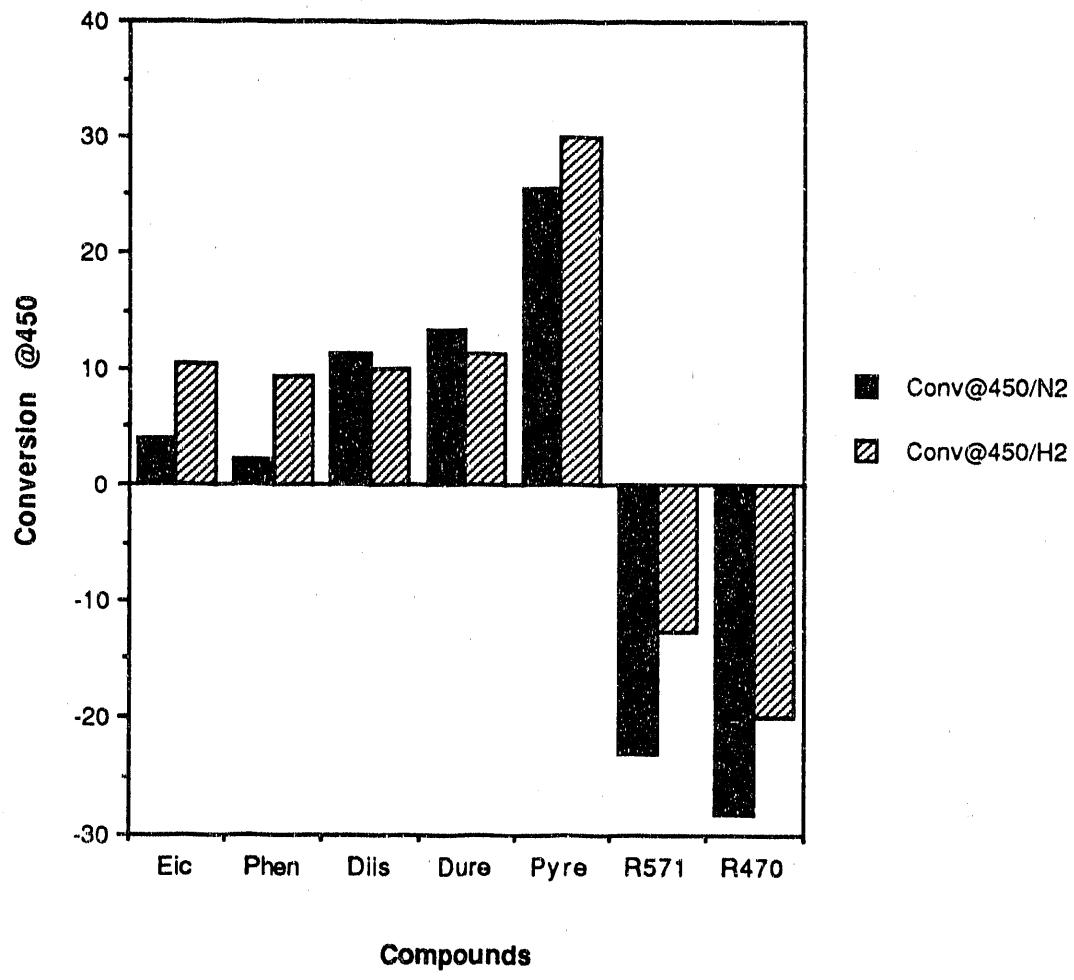


Figure 2. Conversion for PSOC 1448 under N₂ and H₂ at 450°C

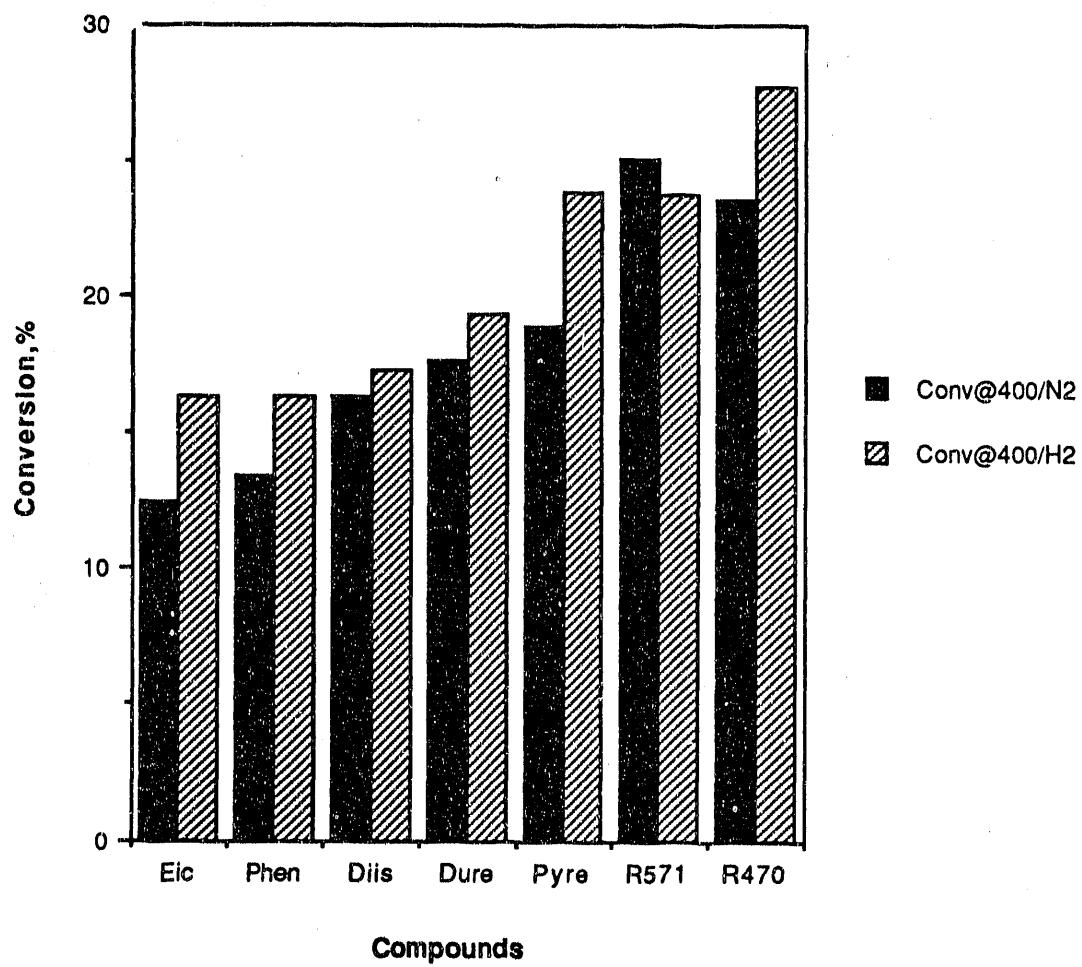


Figure 3. Conversion for PSOC1448 under N_2 and H_2 at 400°C

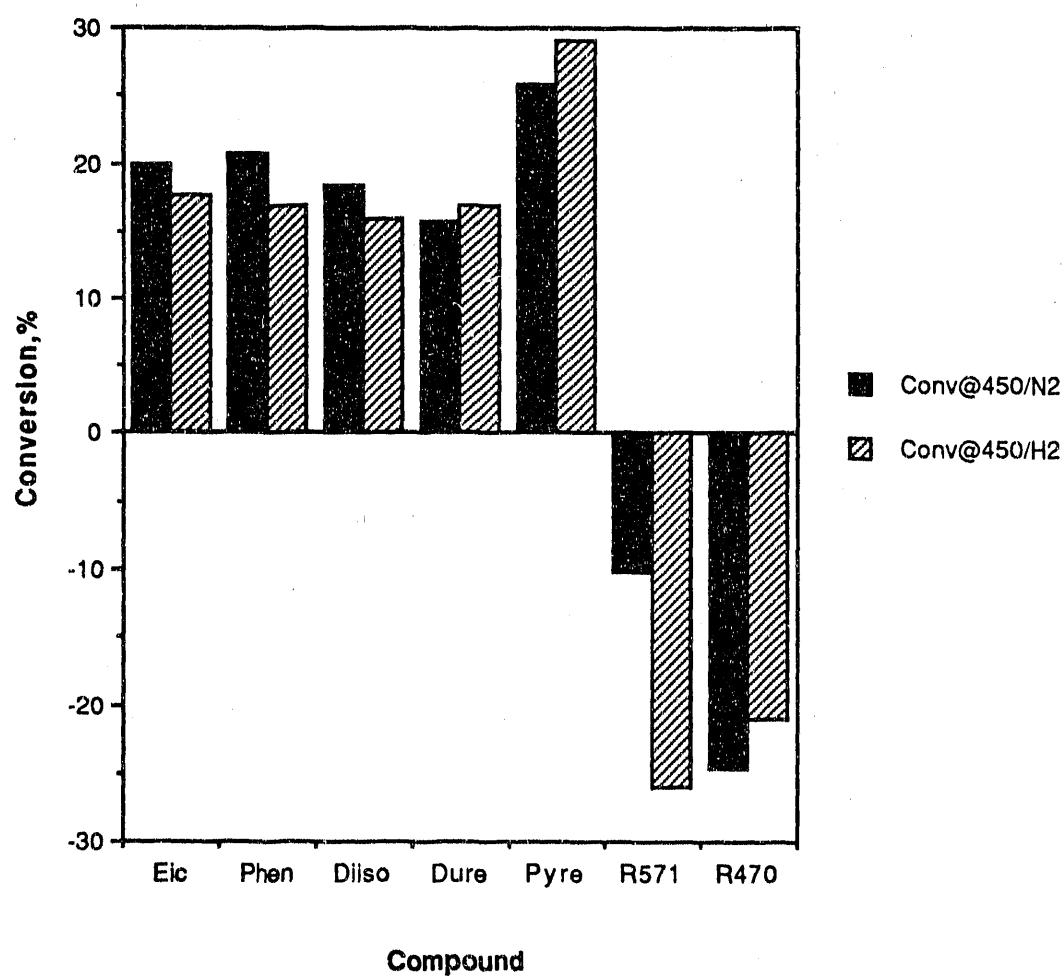


Figure 4. Conversion for PSOC1488 under N_2 and H_2 at 450°C

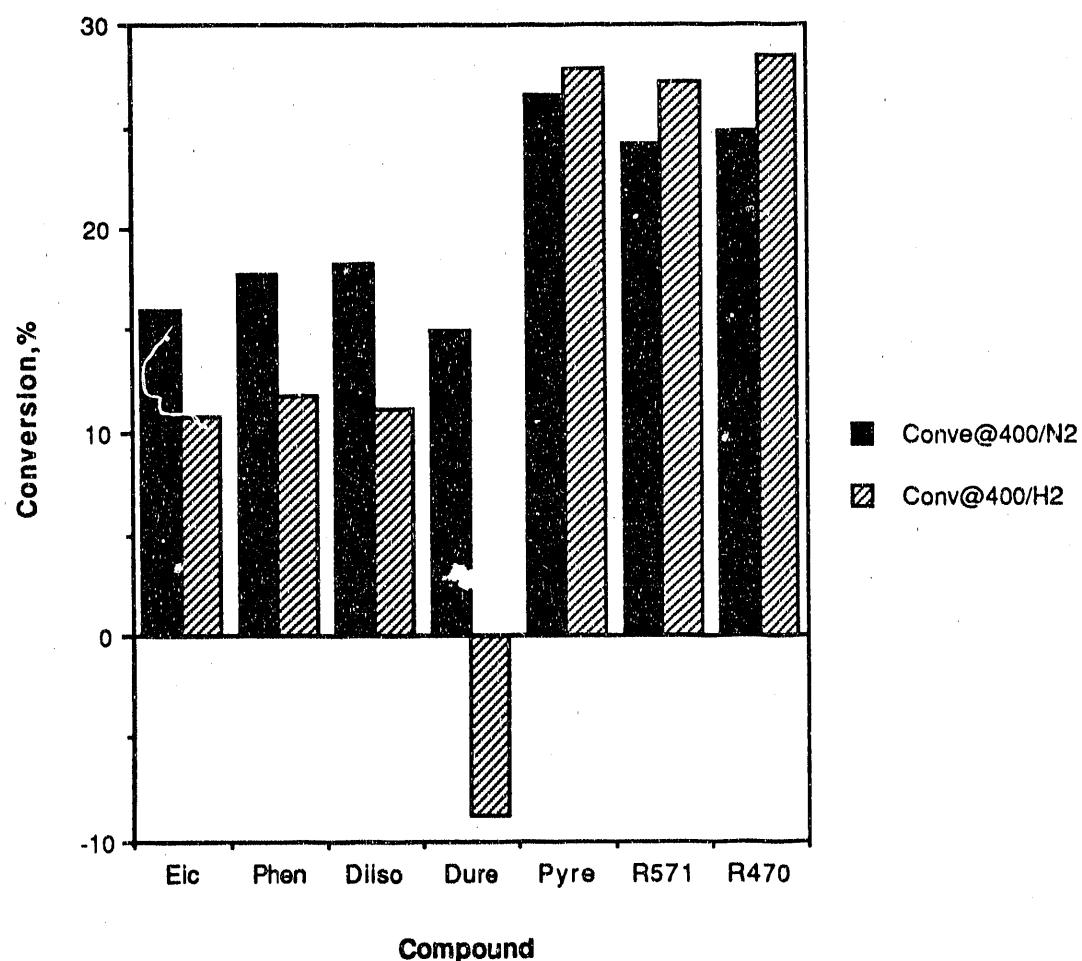


Figure 5. Conversion for PSOC1488 under N_2 and H_2 at 400°C

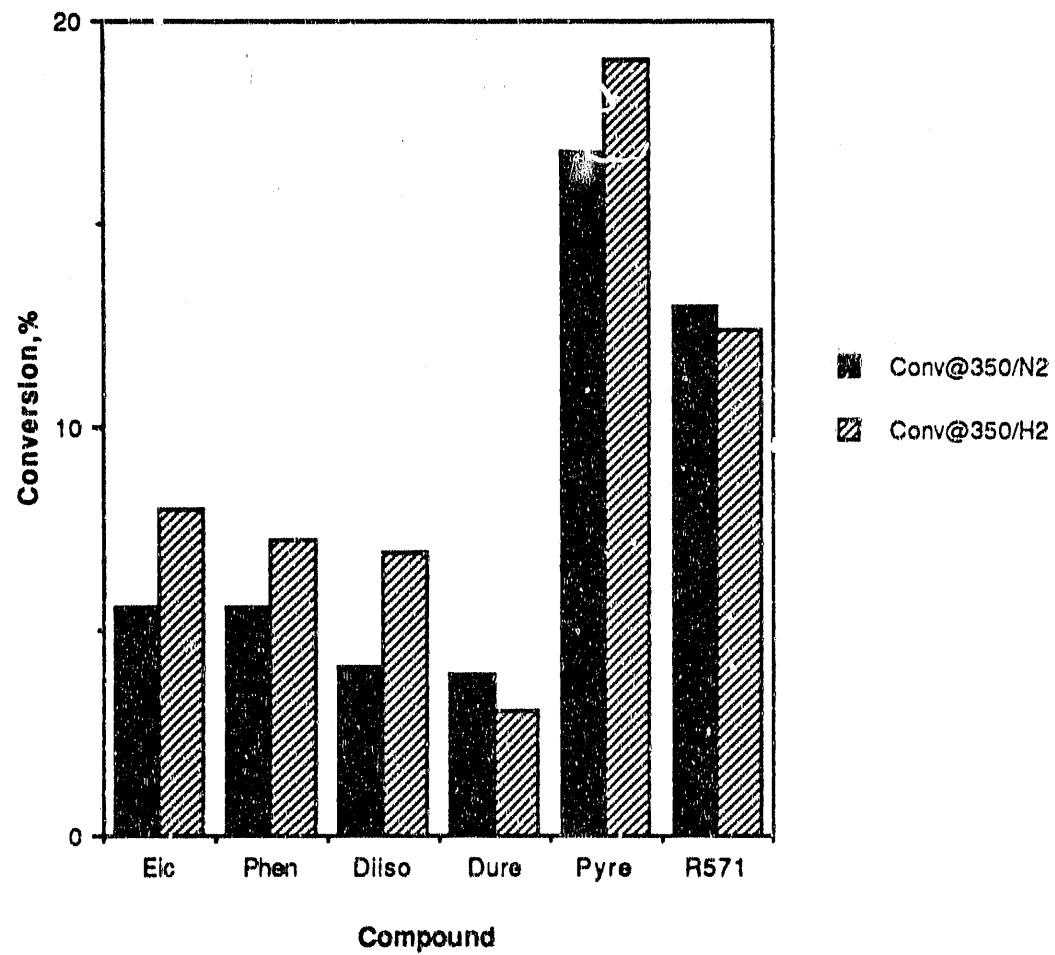


Figure 6. Conversion for PSOC1488 under N₂ and H₂ at 350°C

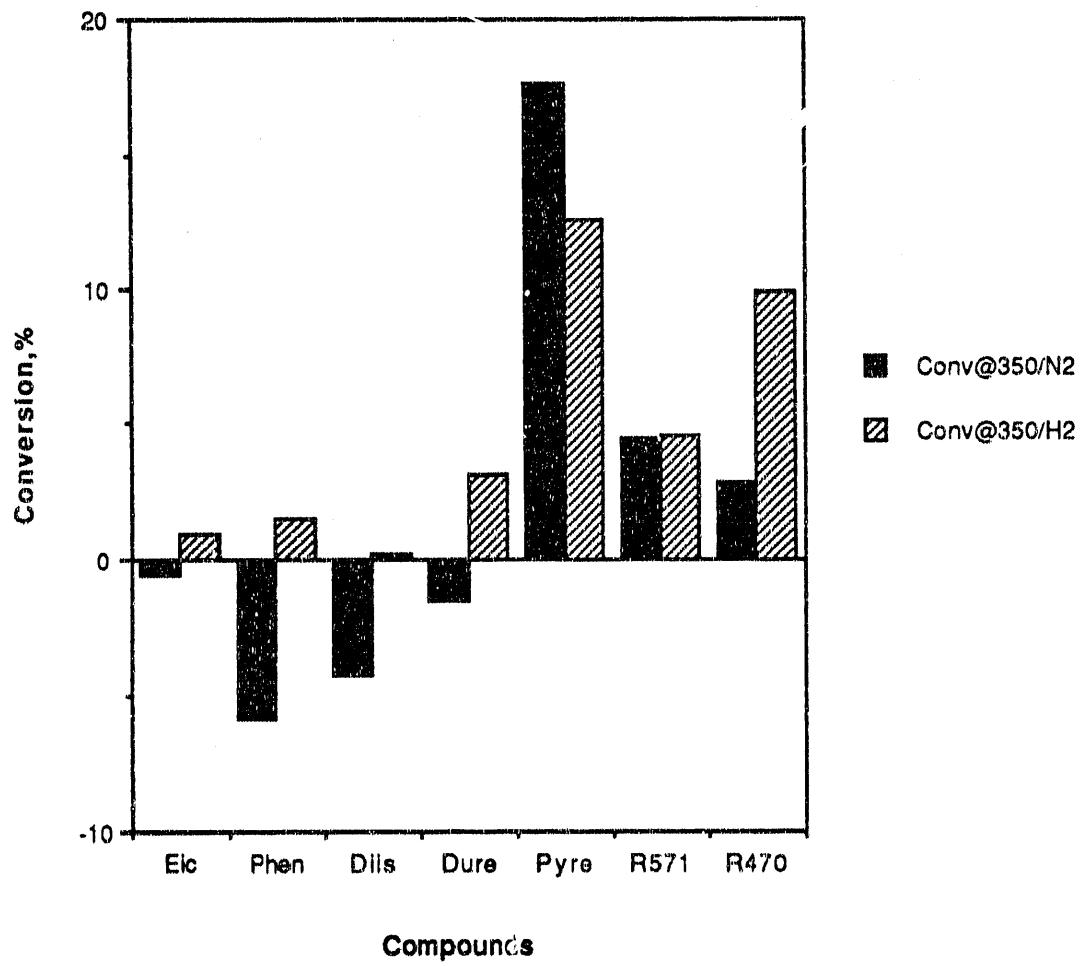


Figure 7. Conversion for PSOC1498 under N_2 and H_2 at 350°C

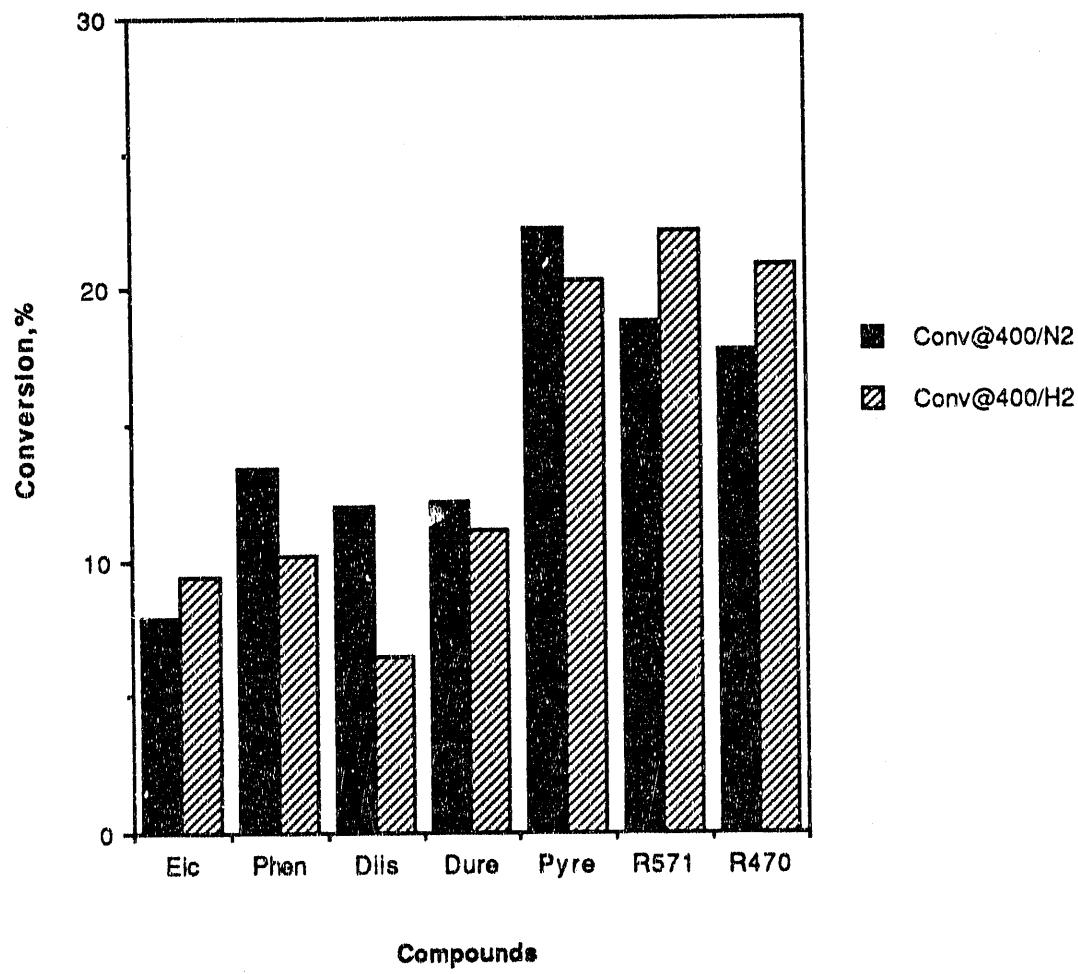


Figure 8. Conversion for PSOC1498 under N_2 and H_2 at 400°C

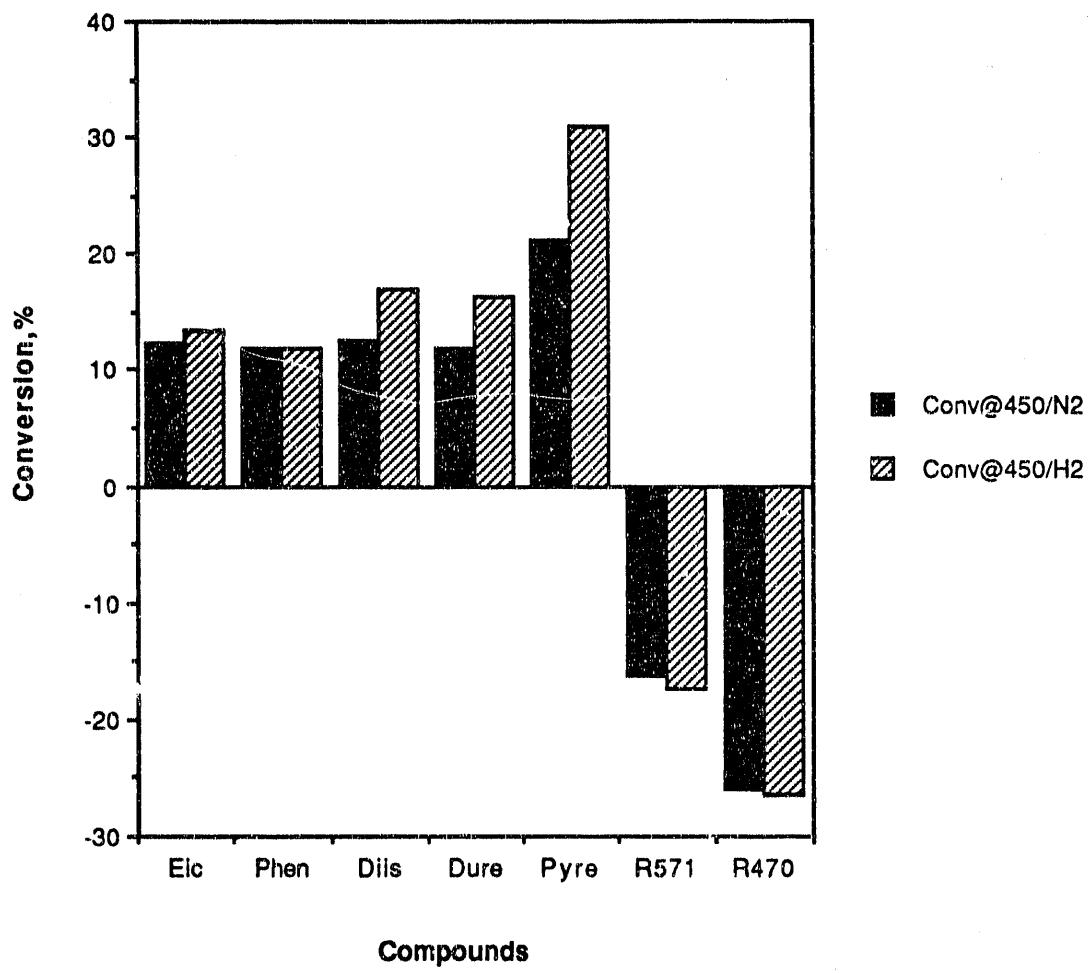


Figure 9. Conversion for PSOC1498 under N_2 and H_2 at 450°C

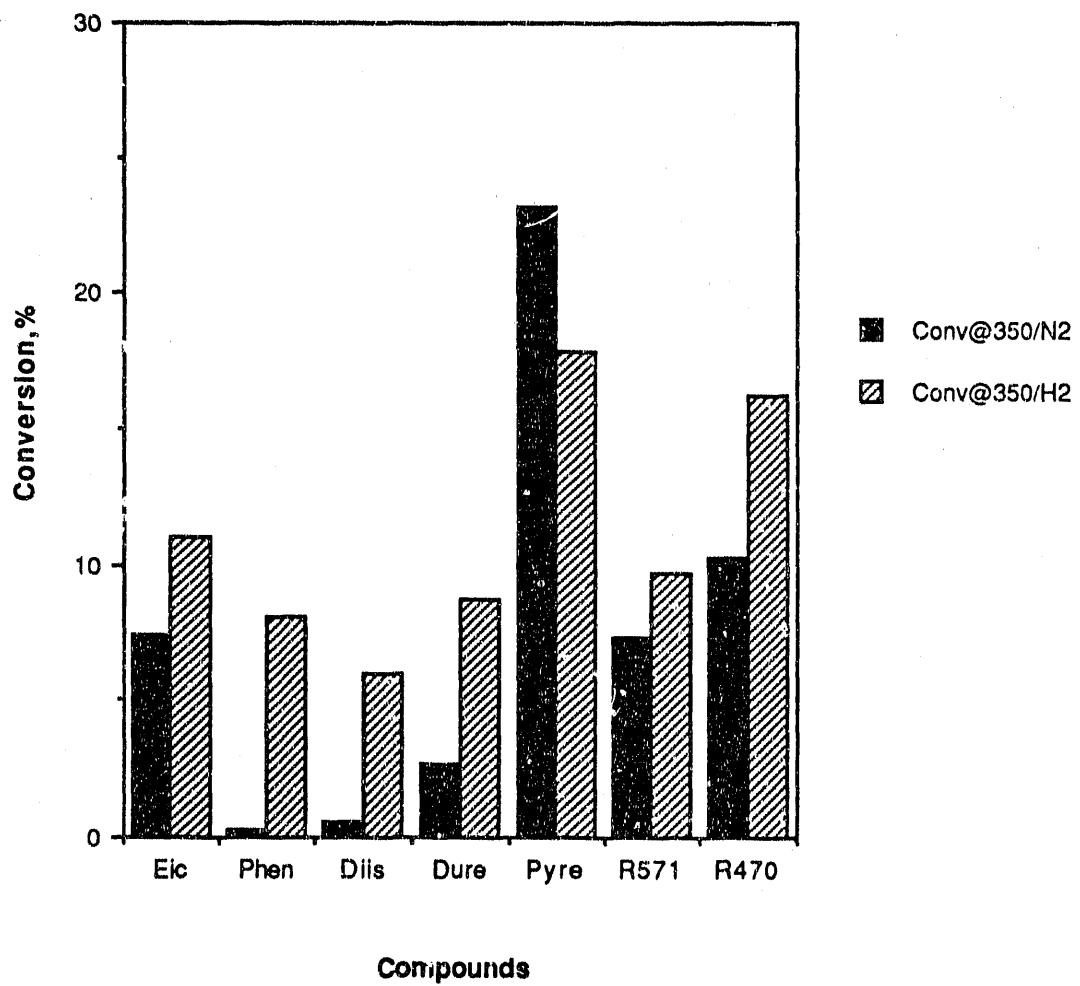


Figure 10. Conversion for PSOC1501 under N_2 and H_2 at 350°C

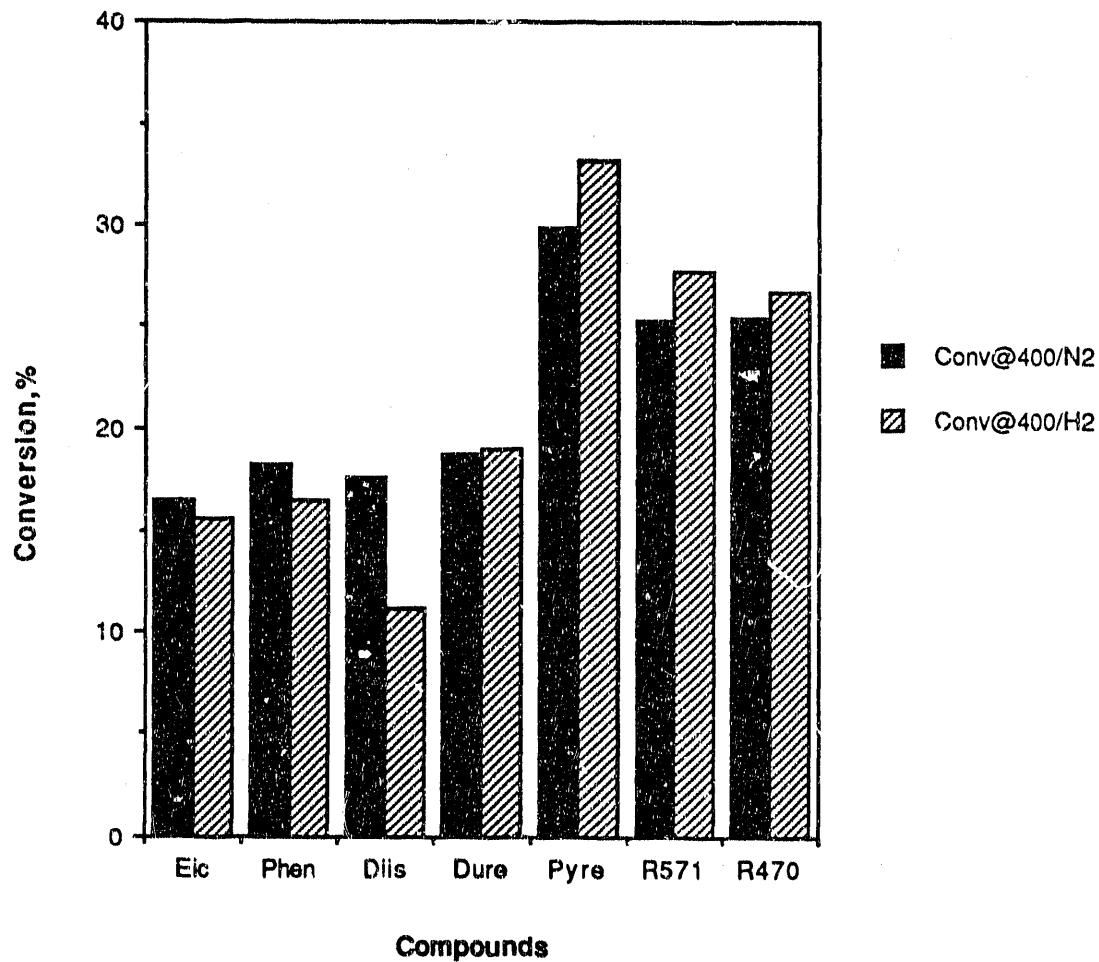


Figure 11. Conversion for PSOC1501 under N_2 and H_2 at 400°C

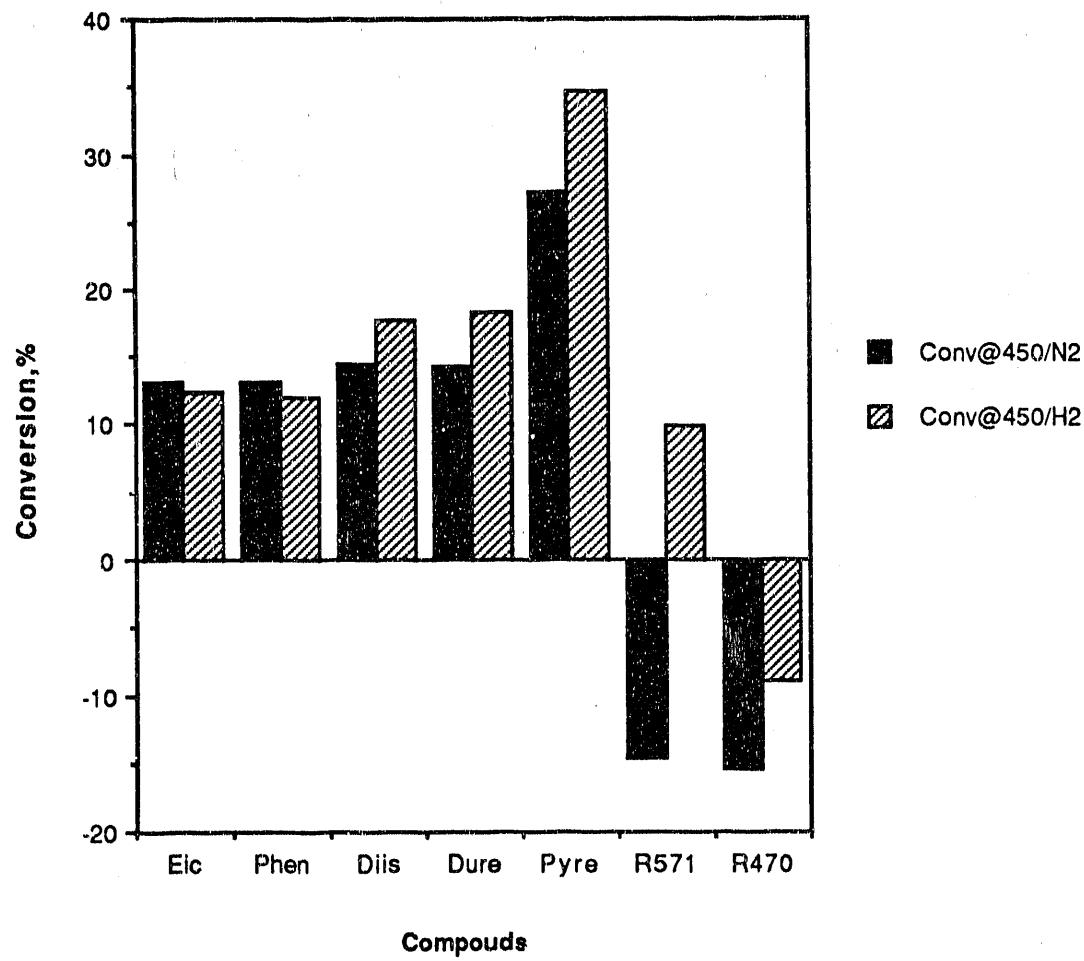


Figure 12. Conversion for PSOC1501 under N_2 and H_2 at 450°C

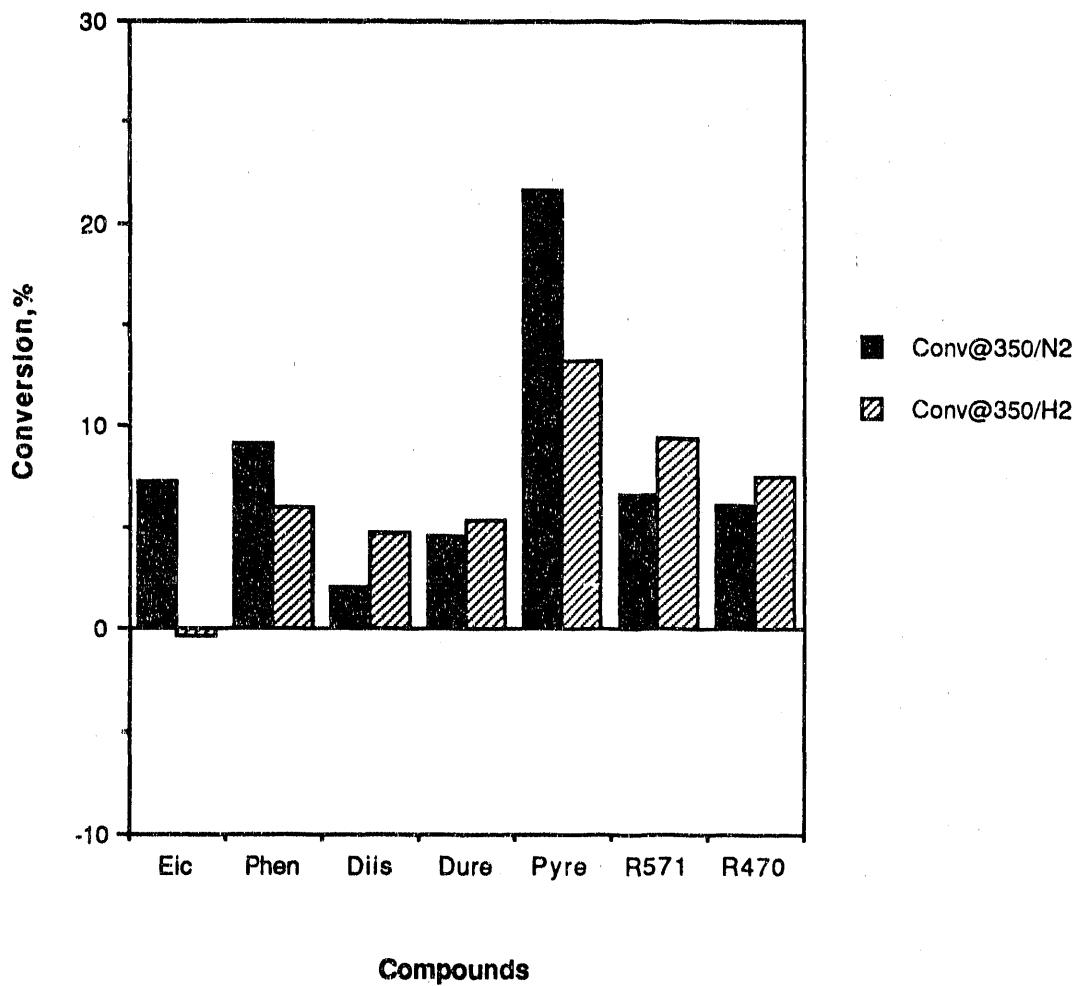


Figure 13. Conversion for PSOC1504 under N₂ and H₂ at 350°C

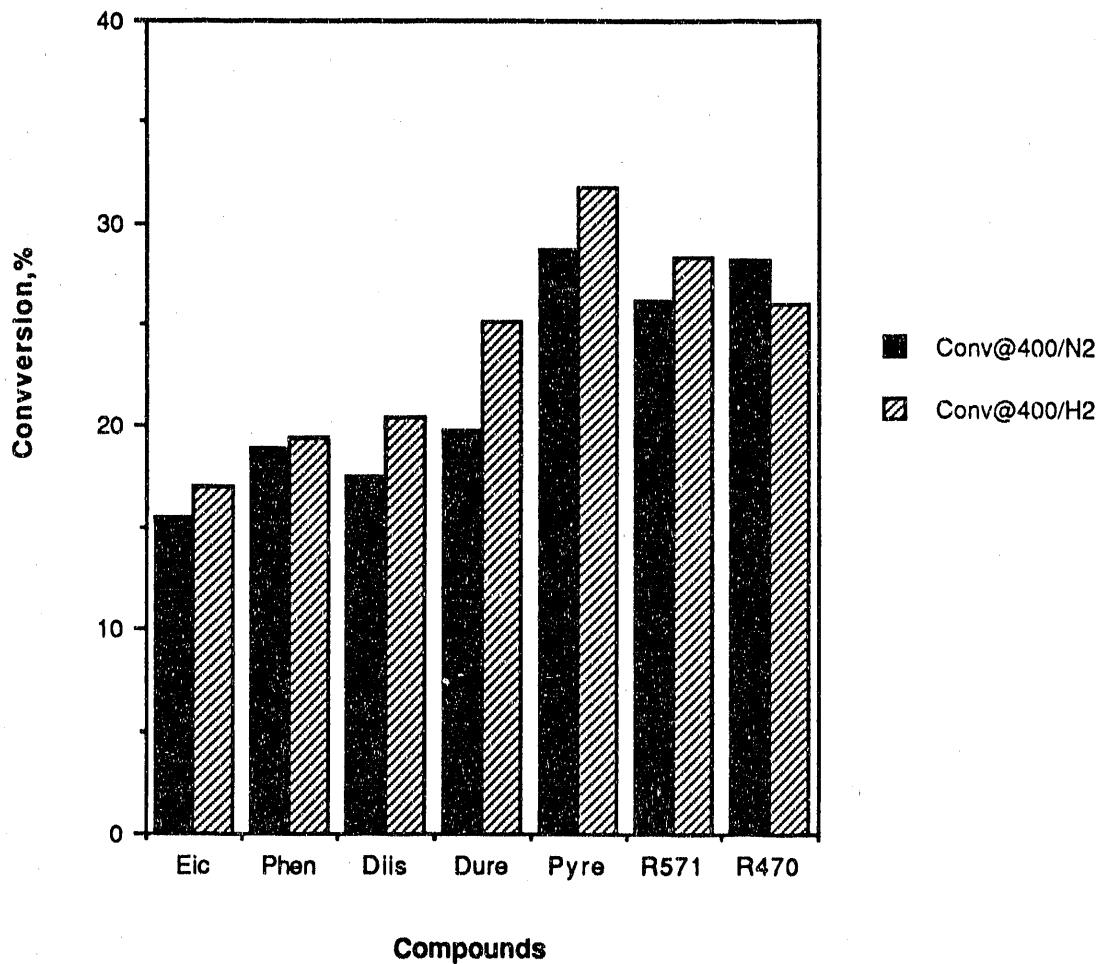


Figure 14. Conversion for PSOC1504 under N₂ and H₂ at 400°C

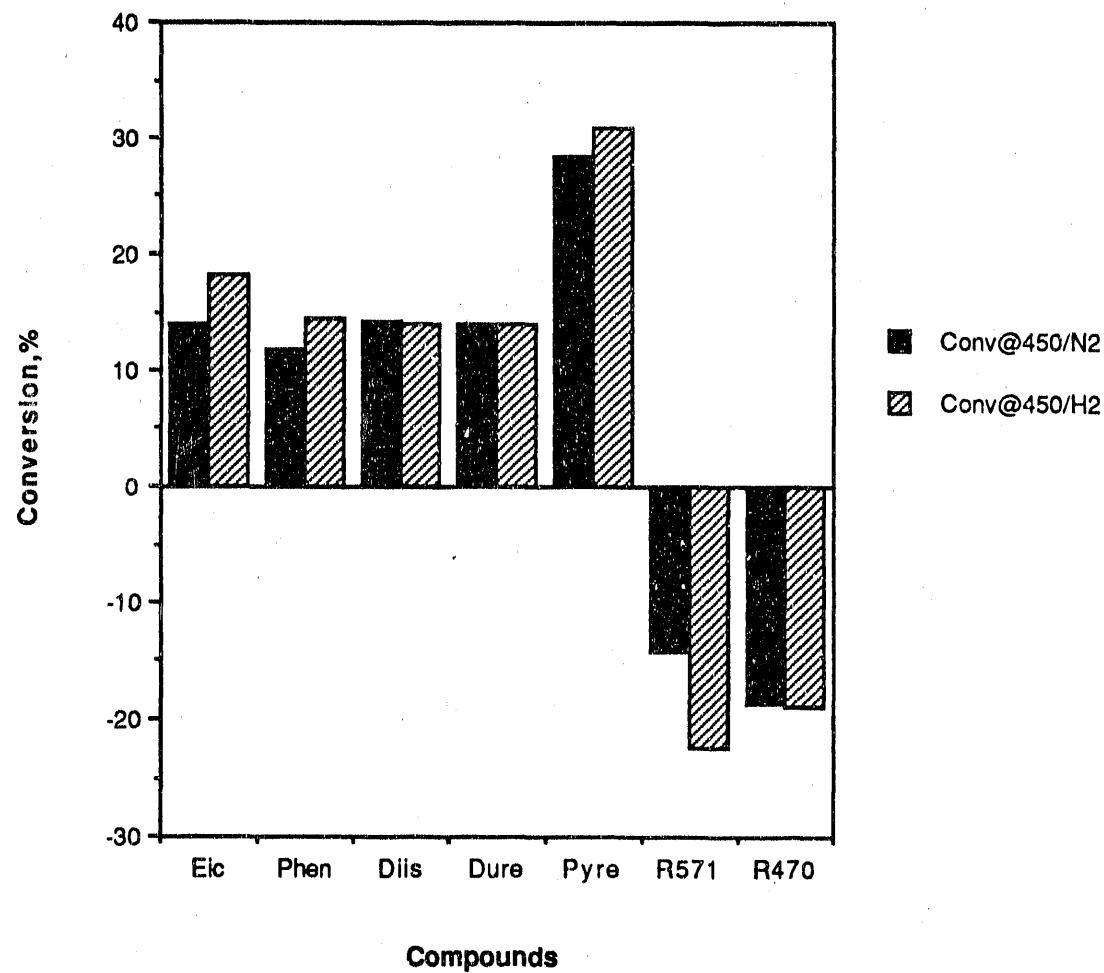


Figure 15. Conversion for PSOC1504 under N_2 and H_2 at 450°C

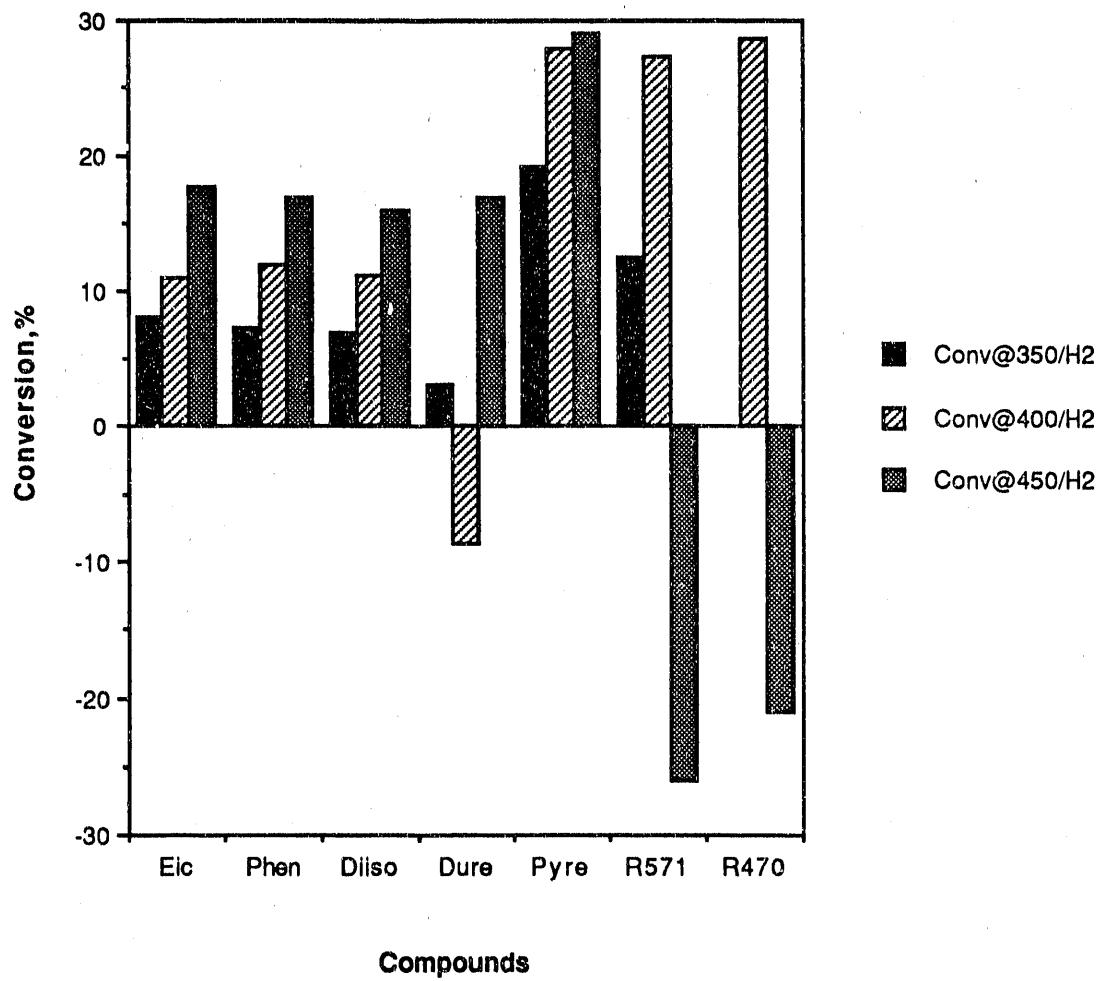


Figure 16. Conversions for PSOC1488;H₂ at three reaction temperatures

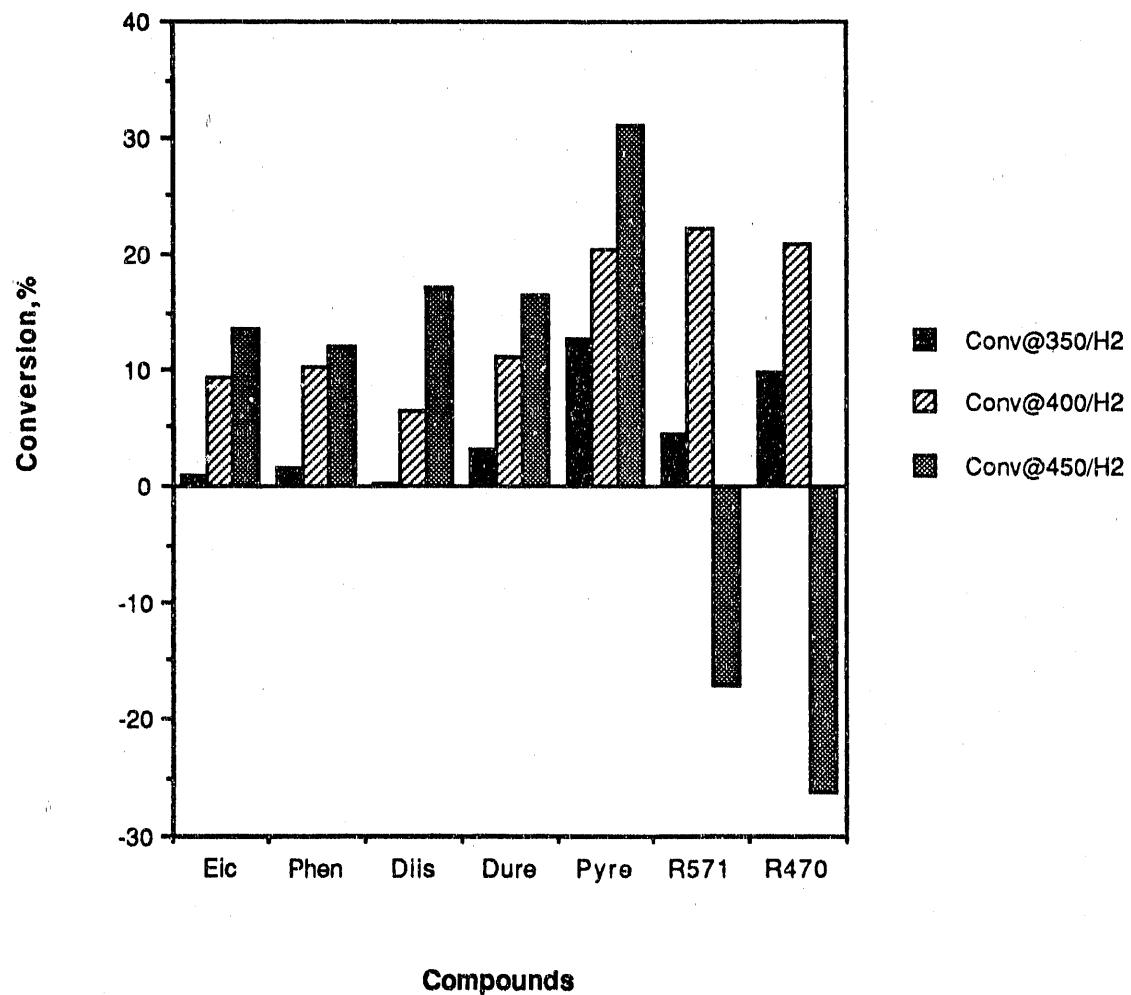


Figure 17. Conversions for PSOC1498; H₂ at three reaction temperatures

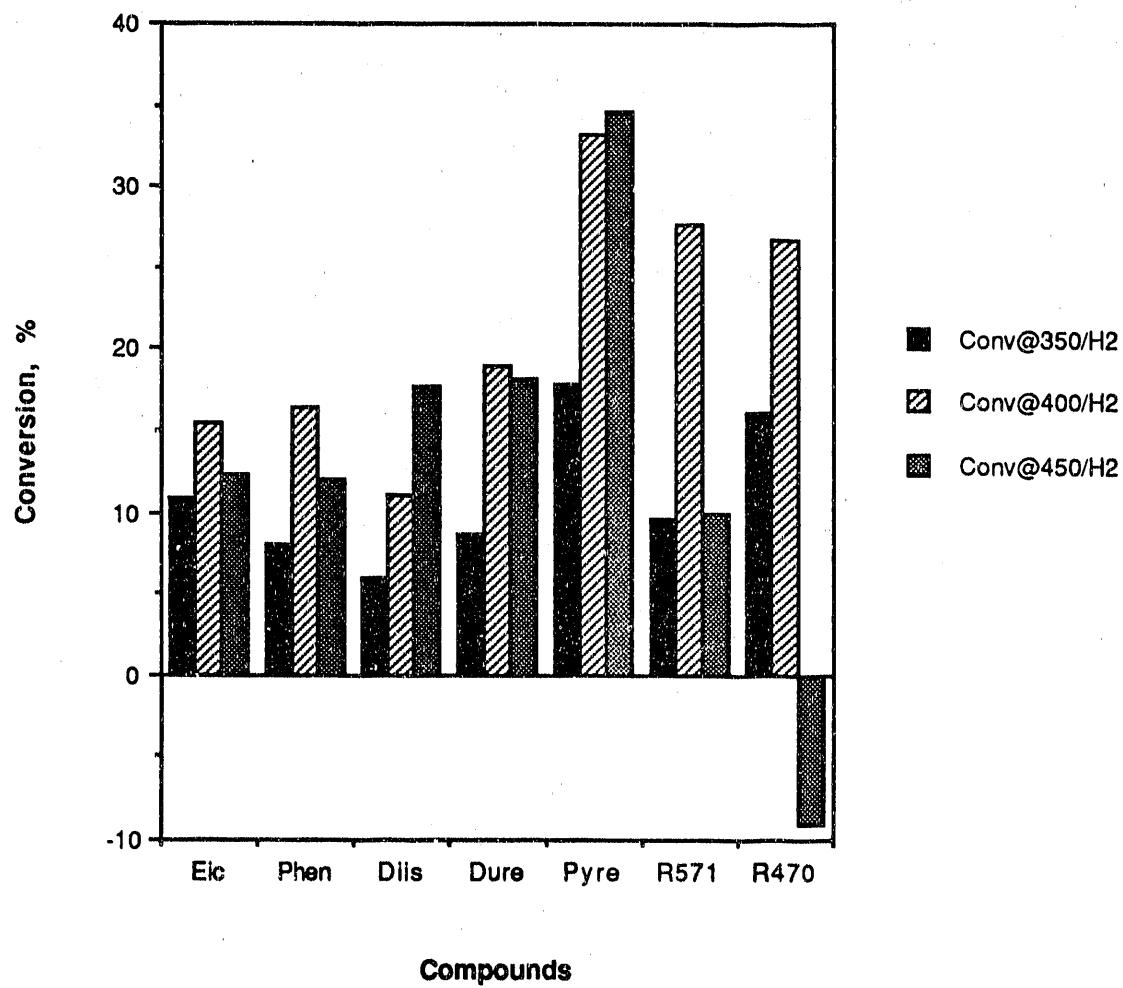


Figure 18. Conversions for PSOC1501; H₂ at three reaction temperatures

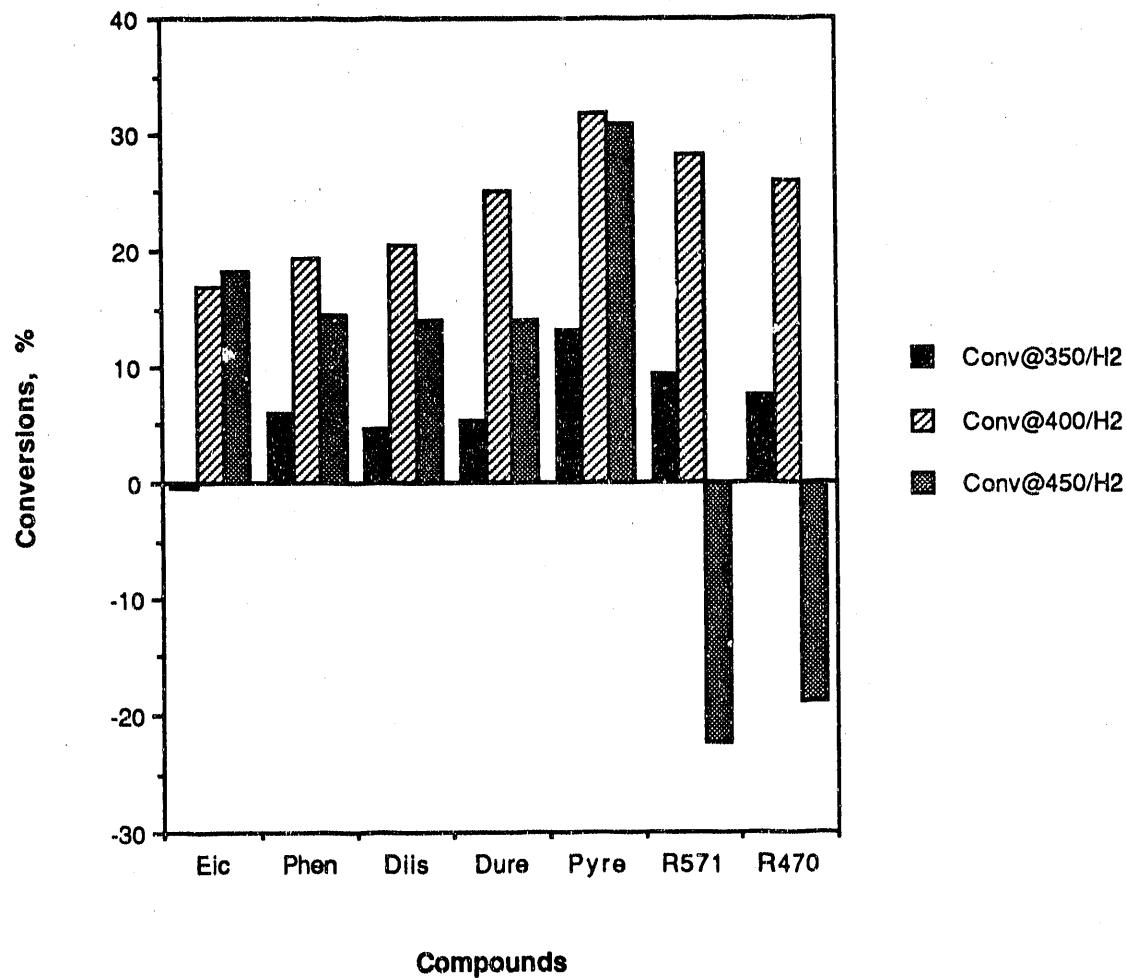


Figure 19. Conversions for PSOC1504; H₂ at three reaction temperatures

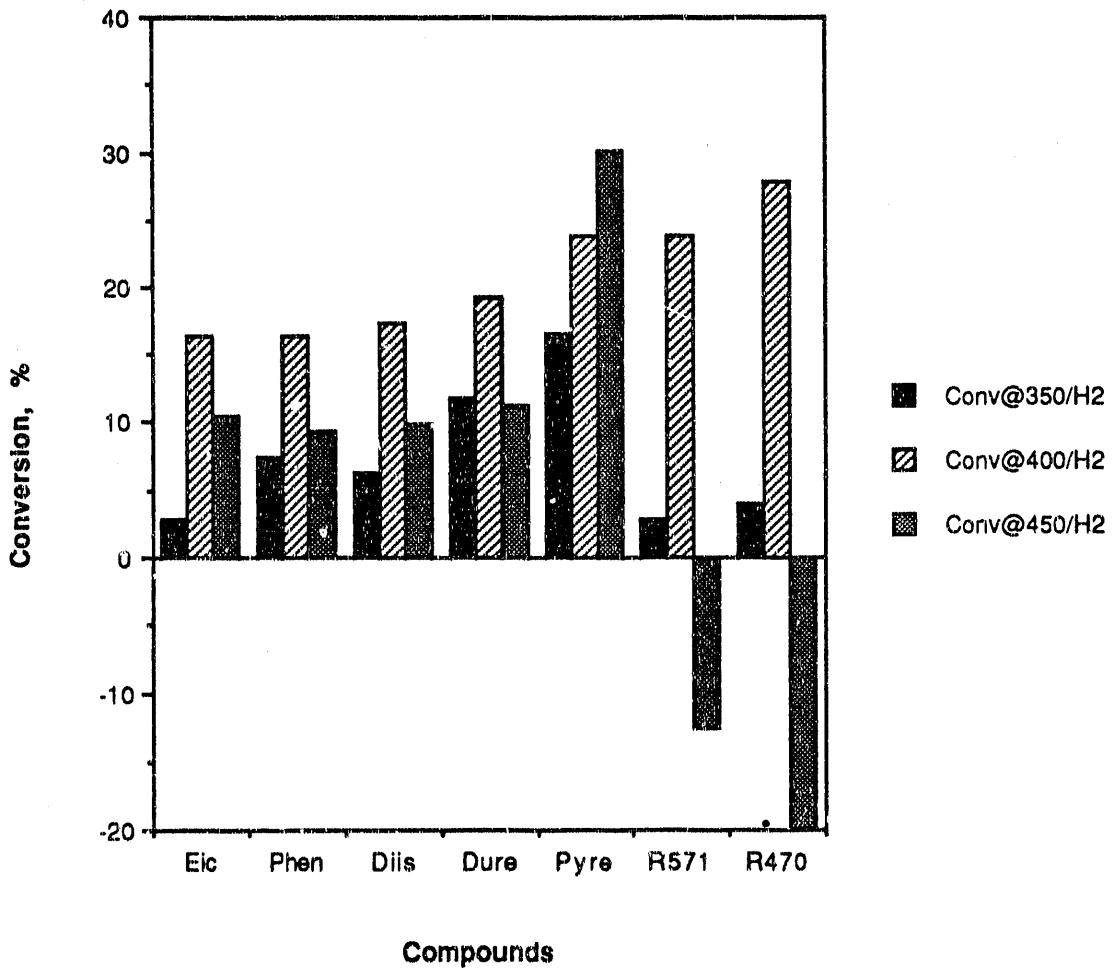


Figure 20. Conversion for PSOC1448;H₂ at three reaction temperatures

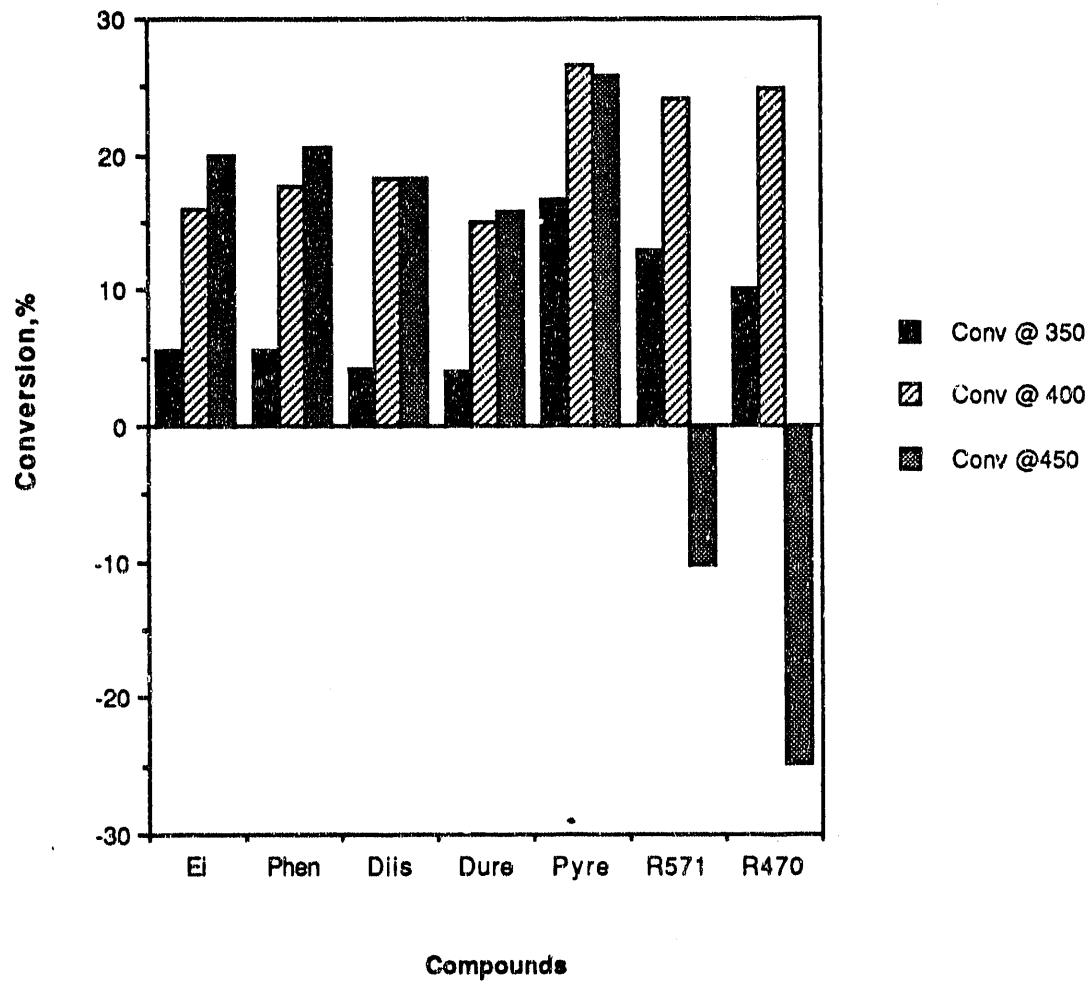


Figure 21. Conversions for PSOC1488; N₂ at three reaction temperatures

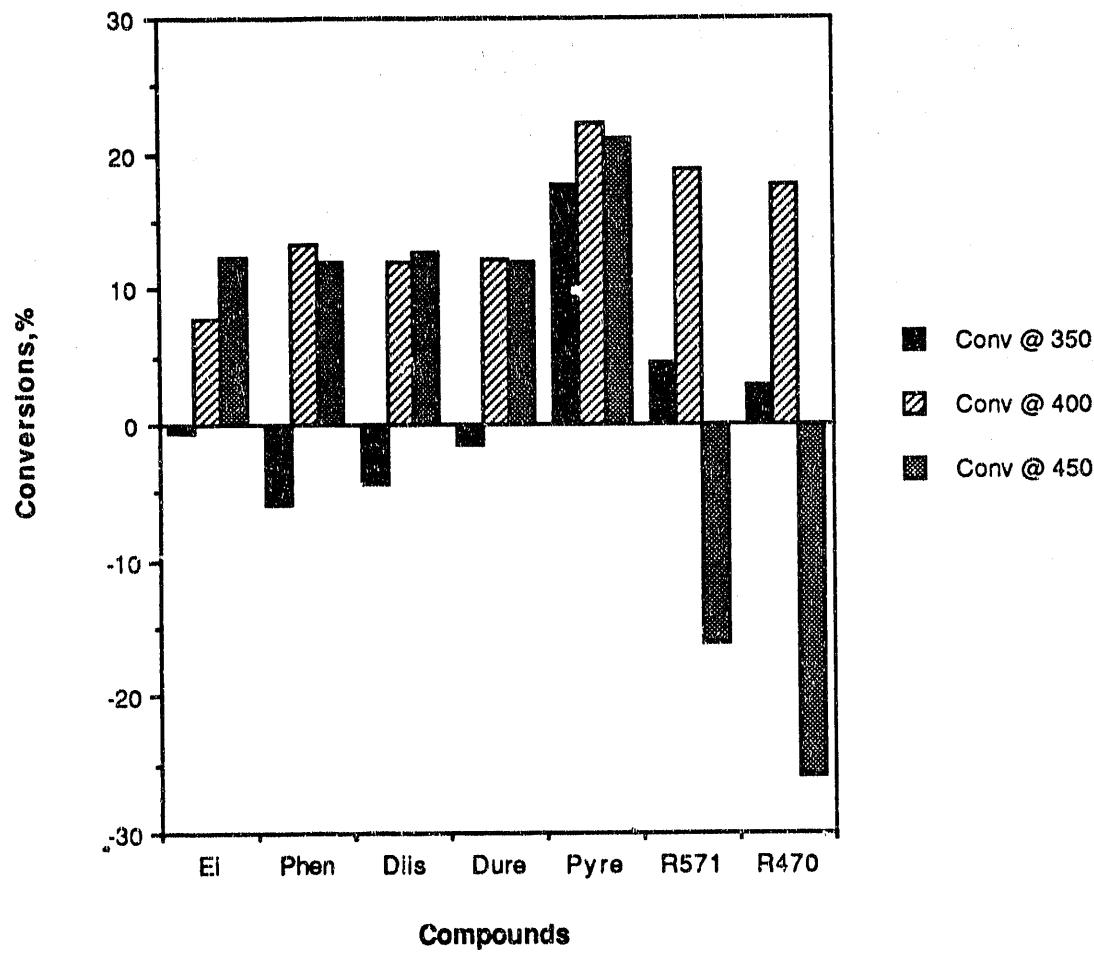


Figure 22. Conversions for PSOC1498; N₂ at three reaction temperatures

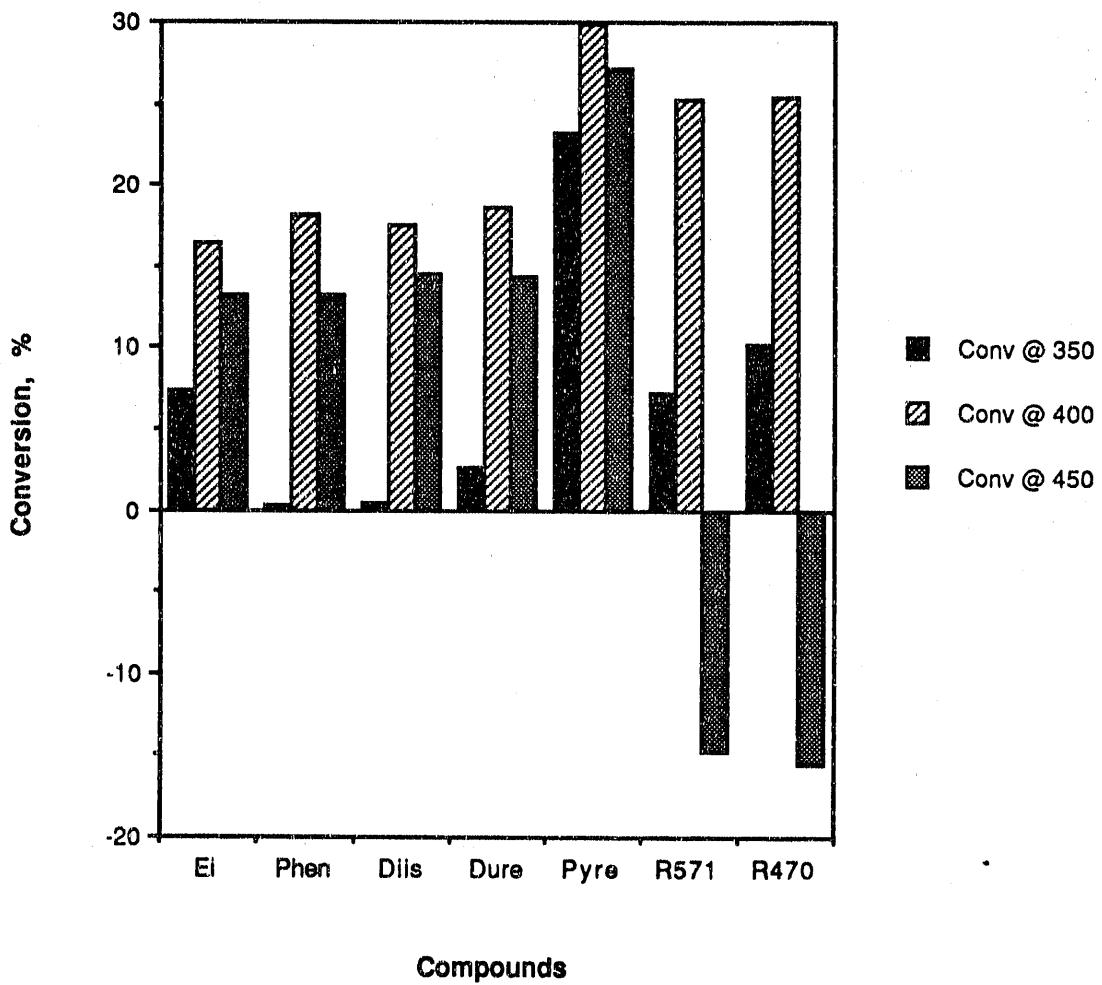


Figure 23. Conversions for PSOC1501, N₂ at three reaction temperatures

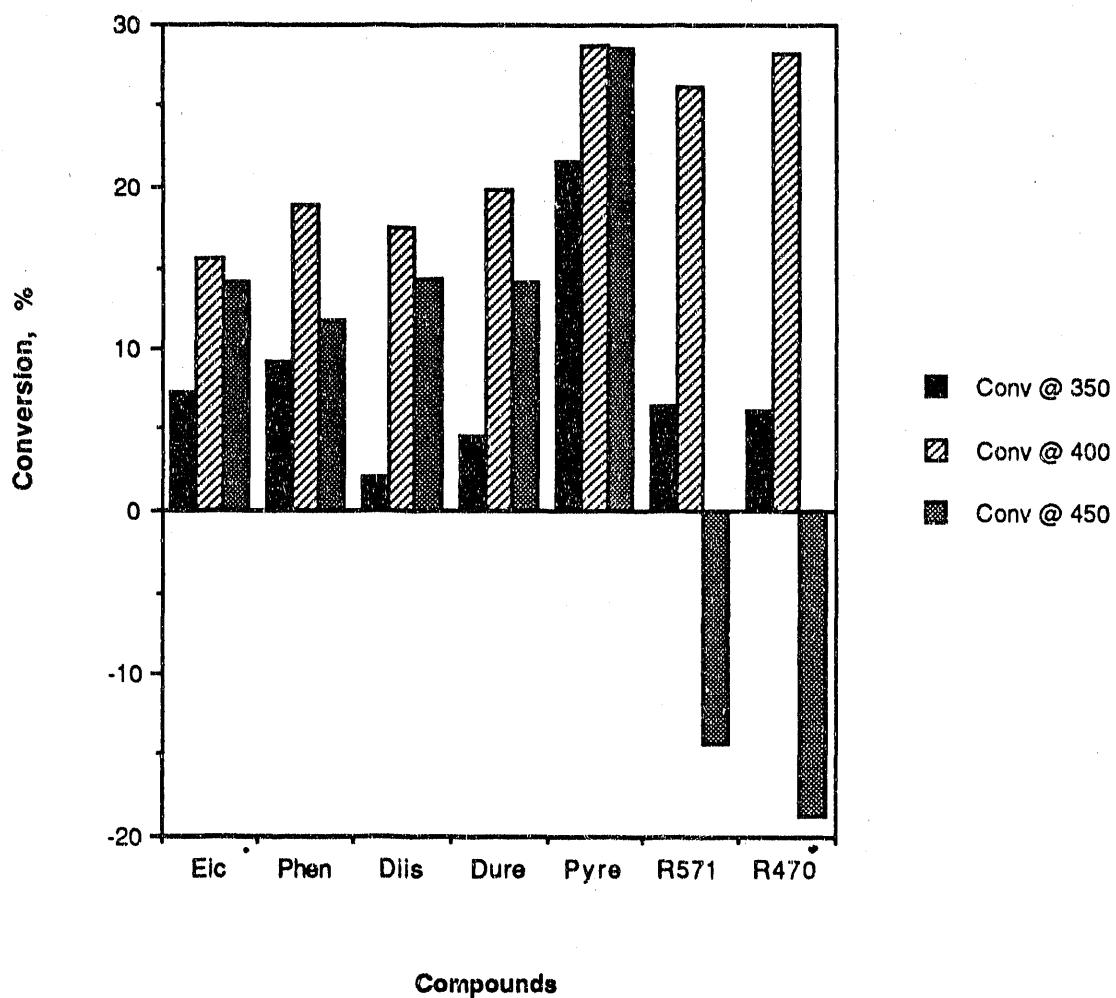


Figure 24. Conversions for PSOC1504; N₂ at three reaction temperatures

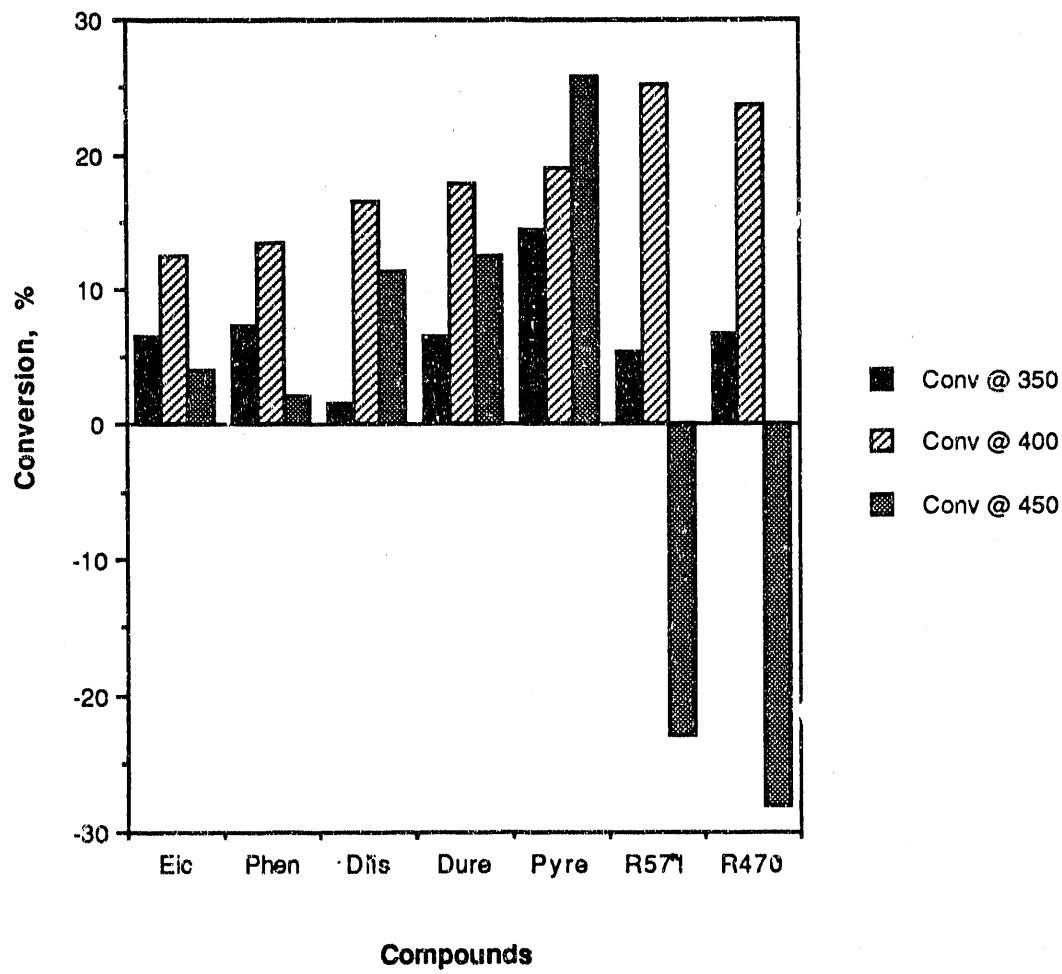


Figure 25. Conversions for PSOC1448, N2 at three reaction temperatures

Literature Cited

- [1] Schobert, H. H., J. Tomic, D. Moyer and, J. McConnie, "Inhibition of Retrogressive Reactions in Coal/Petroleum Co-Processing" U.S.D.O.E. Report, No 88PC-88935-QTR-7, 1990.
- [2] Rhee, Y., J. Guin and, C. W. Curtis, *Fuel Processing Technology*, 22, P97, 1989.

APPENDIX 1

This appendix contains actual data collected in the reactions of coals with five model compounds under hydrogen atmosphere and the comparisons of a vertical and horizontal design microreactor.

T=350 °C H2							T=350 °C H2								
	Wt.MC	PSOC 1488	THF-sol	THF-insol	Wt.daf	THF ext		Wt.MC	PSOC 1498	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol%
J6	Eicosane	5.1194	2.5357	5.606	2.1011	2.28314428	0.30632866	7.895748853	92.02659764						
J7	1-Phenylidod	4.9959	2.5108	5.405	2.0976	2.26072432	0.30332058	4.679005551	92.7844223						
J8	1,4-Diiso	5.0212	2.5063	4.999	2.1011	2.25667252	0.30277696	-14.40071398	93.10611005						
J9	Durene	5.0326	2.5459	3.155	2.1533	2.29232836	0.30756089	-95.32495102	93.93505911						
J10	Pyrene	5.0404	2.516	5.595	1.8341	2.2654064	0.30394878	11.06429396	80.96119089						
J1	Eicosane	4.9781	2.5048	5.37	2.2881	2.26659352	0.31734541	3.28927921	100.9488459						
J2	1-Phenylidod	5.0192	2.5244	5.233	2.2486	2.28432956	0.31982863	-4.641564539	98.43588418						
J3	1,4-Diiso	5.0076	2.5079	4.424	2.2646	2.26939871	0.31773816	-39.71704755	99.78854707						
J4	Durene	5.0908	2.5722	4.7	2.2553	2.32758378	0.32588465	-30.79092807	96.8944714						
J5	Pyrene	5.0343	2.5181	5.664	1.9925	2.27862869	0.31903045	13.63405756	87.44294359						
J11	Eicosane	5.0088	2.5173	5.583	2.0986	2.35745145	0.35288976	9.387690055	89.01986083						
J12	1-Phenylidod	4.9852	2.5226	5.64	2.1715	2.3624149	0.35363275	12.74827933	91.91865493						
J13	1,4-Diiso	5.0002	2.5193	5.656	2.2186	2.35932445	0.35317014	12.750678	94.04386921						
J14	Durene	5.0113	2.5092	5.292	2.144	2.3498658	0.35175426	-3.096102745	91.2392529						
J15	Pyrene	5.0124	2.5075	5.861	1.93	2.34827375	0.35151594	21.16806255	82.1880328						
J16	Eicosane	5.0081	2.5108	5.425	2.3128	2.30466332	0.39235586	1.064977182	100.3530529						
J17	1-Phenylidod	4.972	2.5014	5.492	2.1596	2.29603506	0.39088695	5.623304847	94.05779718						
J18	1,4-Diiso	4.9916	2.5077	4.893	2.1937	2.30181783	0.39187143	-21.3080039	95.30293716						
J19	Durene	4.9895	2.4965	4.21	2.1686	2.29153735	0.39012124	-51.04089792	94.63515836						
J20	Pyrene	5.0195	2.5059	5.733	1.9963	2.30016561	0.39159015	13.99507265	86.78940296						
J21	Eicosane	5.0099	2.5061	5.029	2.2358	2.3031059	0.53581415	-22.4355364	97.0776029						
J22	1-Phenylidod	4.9666	2.5877	5.494	2.2019	2.3780963	0.55326056	-1.087447932	92.59086775						
J23	1,4-Diiso	4.9906	2.5095	4.957	2.1603	2.3062305	0.53654109	-24.72177381	93.67233674						
J24	Durene	5.0148	2.5079	5.238	2.0326	2.3047601	0.536199	-13.58054582	88.19139137						
J25	Pyrene	5.0028	2.577	5.977	1.9744	2.368263	0.55097286	17.65965788	83.36911905						

		T=400 °C H2							
		Wt.MC	PSOC 1488	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
J26	Eicosane	4.9965	2.5087	5.397	2.0802	2.33208752	0.45245012	-2.227622918	89.19905373
J27	1-Phenylidod	4.9718	2.5066	5.172	2.0563	2.33013536	0.45207138	-10.80930234	88.24809216
J28	1,4-Diiso	4.9991	2.5005	5.098	2.0661	2.3244648	0.45097123	-15.14633503	88.88497688
J29	Durene	4.9885	2.503	4.949	2.5288	2.3267888	0.45142211	-21.09869651	108.6819741
J30	Pyrene	5.0152	2.5008	5.653	1.678	2.32474368	0.45102533	8.034204789	72.18000051
		Wt.MC	PSOC 1498	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
J31	Eicosane	5.0094	2.509	5.291	2.0865	2.3040147	0.43500131	-6.65800059	90.55931805
J32	1-Phenylidod	4.9787	2.5058	5.395	2.0673	2.30107614	0.43444651	-0.788609626	89.84057346
J33	1,4-Diiso	4.9945	2.0113	4.897	1.7276	1.84697679	0.34871189	-24.15904171	93.53663832
J34	Durene	4.9883	2.5056	4.3843	2.0459	2.30089248	0.43441183	-45.13082822	88.91767076
J35	Pyrene	5.0135	2.5094	5.725	1.8354	2.30438202	0.43507066	11.9958121	79.64825207
		Wt.MC	PSOC 1501	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
J36	Eicosane	5.0086	2.508	5.614	1.9843	2.348742	0.68487586	-3.383762968	84.48352352
J37	1-Phenylidod	4.9646	2.5071	5.485	1.9608	2.34789915	0.68463009	-6.994767776	83.51295668
J38	1,4-Diiso	4.9898	2.5086	5.462	2.0875	2.3493039	0.68503971	-9.059692443	88.85610755
J39	Durene	5.0039	2.5099	5.205	1.905	2.35052135	0.68539471	-20.60371446	81.04584968
J40	Pyrene	5.0113	2.5035	6.012	1.5655	2.34452775	0.68364702	13.5231064	66.77250888
		Wt.MC	PSOC1504	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
J41	Eicosane	5.0912	2.5178	5.73	1.9188	2.31108862	0.62413339	0.63461918	83.02580798
J42	1-Phenylidod	4.9677	2.5141	5.703	1.8598	2.30769239	0.6232162	4.856964437	80.59133046
J43	1,4-Diiso	4.99	2.511	5.565	1.8345	2.3048469	0.62244775	-2.058607333	79.59313914
J44	Durene	5.0111	2.5108	5.385	1.7259	2.30466332	0.62239817	-10.78240659	74.88729417
J45	Pyrene	5.0161	2.513	6.002	1.5737	2.3066827	0.62294352	15.73499797	68.22351423
		Wt.MC	PSOC1448	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
J46	Eicosane	5.0128	2.5016	6.73	1.8433	2.20190832	0.79000228	42.10882504	83.71374881
J47	1-Phenylidod	4.9764	2.5053	5.816	1.8444	2.20516506	0.79117073	2.196174211	83.63999745
J48	1,4-Diiso	4.983	2.5074	5.777	1.8253	2.20701348	0.79183391	0.098145702	82.70452431
J49	Durene	4.9991	2.5169	5.659	1.7872	2.21537538	0.794834	-6.090796212	80.67255853
J50	Pyrene	5.0215	2.5121	6.069	1.6836	2.21115042	0.79331817	11.49545649	76.14135994

	T=450 °C H2						
	Wt.MC	PSOC1488	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %
J51	Eicosane	5.0043	2.5104	4.224	1.8781	2.27768592	-46.15186974
	1-Phenylidod	4.9829	2.5318	3.12	1.9113	2.29710214	-92.9912455
J52	1,4-Diiso	5.0084	2.5146	5.309	1.9228	2.28149658	1.282147157
J53	Durene	5.0192	2.5144	5.109	1.8995	2.28131512	0.27132627
J54	Pyrene	5.0041	2.5202	5.562	1.6225	2.28657746	-7.957089009
							83.26337661
							70.95757867
J56	Eicosane	5.0074	2.5035	3.914	1.9468	2.2506465	0.30303684
J57	1-Phenylidod	4.9735	2.5115	3.121	1.9732	2.2578385	0.3040052
J58	1,4-Diiso	5.013	2.5212	4.889	1.8781	2.2665588	0.30517934
J59	Durene	5.016	2.5086	4.823	1.8853	2.2552314	0.30365417
J60	Pyrene	5.0756	2.5036	5.771	1.5511	2.2507364	0.30304894
							17.43211957
							68.91522259
J61	Eicosane	5.0846	2.501	5.424	2.0414	2.3279308	0.39127847
J62	1-Phenylidod	4.9984	2.5083	2.945	2.0425	2.32143165	0.39242055
J63	1,4-Diiso	5.0203	2.4187	5.306	1.8517	2.25132596	0.37840274
J64	Durene	5.0061	2.509	4.765	1.9098	2.3353772	0.39253006
J65	Pyrene	5.0237	2.5043	5.997	1.5239	2.33100244	0.39179475
							24.94657385
							65.37530694
J66	Eicosane	5.0124	2.5113	4.486	1.8769	2.29306803	0.45694982
J67	1-Phenylidod	4.9948	2.5064	3.329	1.9568	2.28859384	0.45605823
J68	1,4-Diiso	5.0261	2.5123	4.53	1.9727	2.29398113	0.45713178
J69	Durene	5.0103	2.5183	5.081	1.98	2.29945973	0.45822352
J70	Pyrene	5.0225	2.5171	5.61	1.588	2.29836401	0.45800517
							5.634217492
							69.09262384
J71	Eicosane	5.0155	2.5264	4.276	1.9911	2.22272672	0.61376271
J72	1-Phenylidod	4.9999	2.538	3.333	2.0259	2.2329324	0.61656081
J73	1,4-Diiso	5.0156	2.5085	5.169	1.9875	2.2069783	0.60941409
J74	Durene	5.019	2.5227	4.991	1.97	2.21947146	0.61286383
J75	Pyrene	5.0168	2.5157	5.962	1.5473	2.21331286	0.61116325
							15.09216 33
							69.90877919

VERTICAL VS. HORIZONTAL TUBING BOMB
T=400°C N₂

	Wt/MC	PSOC 1501	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
2V	Eicosane	5.014	2.5128	5.605	1.9895	2.3482116	0.66251409	-3.045470571
2H	Eicosane	5.0215	2.5211	5.427	1.974	2.35596795	0.66470244	-11.00195084
4V	1,4-Diiso	5.0233	2.5774	5.198	1.9731	2.4085803	0.67954625	-20.96032475
4H	1,4-Diiso	5.0171	2.518	1.362	1.9742	2.353071	0.6638851	-183.5467397
6V	Pyrene	5.0206	2.5216	5.79	1.6883	2.3564352	0.66483426	4.437454357
6H	Pyrene	5.0211	2.4075	5.495	1.6102	2.24980875	0.63475115	-7.149547529

T=400°C H₂

	Wt/MC	PSOC 1501	THF-sol	THF-insol	Wt.daf	THF ext	Yield sol %	Yield insol %
1V	Eicosane	5.0068	2.517	5.669	1.9322	2.3521365	0.68733355	-1.068541324
1H	Eicosane	5.0057	2.5285	5.83	1.8633	2.36288325	0.69047393	5.663676771
3V	1,4-Diiso	5.0203	2.5182	5.5272	1.9756	2.3532579	0.68766124	-7.681318835
3H	1,4-Diiso	5.0119	2.5355	5.572	1.9516	2.36942475	0.69238547	-5.583020341
5V	Pyrene	4.993	2.5577	5.881	1.5445	2.39017065	0.69844776	7.930489647
5H	Pyrene	5.0154	2.5199	5.788	1.4819	2.35484655	0.68812547	3.587262518

APPENDIX 2

This Appendix contains the actual data collected in thermal reactions of the resids the reactions of the coals with the two petroleum resids.

COAL + RESID

T=350°C p=500psi N2

Exp#	PSOC	Wt. coal	Wt. FHC-571	THF-sol	THF-insol	daf	THFext	Yield sol%	Yield insol%
D59	1488	2.5053	4.974	6.261	2.0206	2.32116045	0.275420404	43.58076997	87.05128506
D60	1498	2.5102	5.251	6.426	2.1792	2.2817718	0.334350509	36.84196163	95.50473014
D61	1501	2.5216	5.119	5.327	2.185	2.3564352	0.367220561	-6.756840207	92.72480737
D62	1504	2.5063	5.052	6.192	2.1442	2.29476828	0.381249314	33.06437049	93.43862815
D63	1448	2.5026	4.954	6.165	2.0852	2.20178748	0.450749933	34.52876692	94.70487133

T=400°C p=500psi N2

Exp #	PSOC	Wt. coal	Wt. FHC-571	THF-sol	THF-insol	daf	THFext	Yield sol%	Yield insol%
D64	1488	2.5141	5.029	5.853	1.7658	2.32931365	0.318582464	21.69813138	75.80773847
D65	1498	2.5112	5.125	6.458	1.8532	2.283408	0.422678481	39.86679205	81.15938982
D66	1501	2.5052	5.002	6.069	1.7491	2.3411094	0.617246884	19.21111058	74.71244189
D67	1504	2.5113	4.985	5.784	1.6991	2.3009028	0.617877535	7.871799921	73.8449273
D68	1448	2.5134	5.024	6.34	1.657	2.21128932	0.66178014	29.58544839	74.93365907

T=450°C p=500psi N2

Exp #	PSOC	Wt. coal	Wt. FHC-571	THF-sol	THF-insol	daf	THFext	Yield sol%	Yield insol%
D69	1488	2.5096	4.841	2.935	2.5626	2.3251444	0.197883786	-90.48400546	110.2125098
D70	1498	2.5085	4.923	2.678	2.6481	2.2802265	0.261888186	-109.9403145	116.1331999
D71	1501	2.5066	5.135	2.906	2.6868	2.3424177	0.357577113	-110.4233934	114.7020021
D72	1504	2.5103	5.06	3.742	2.6268	2.29843068	0.521231881	-80.02120303	114.2866749
D73	1448	2.5086	5.053	3.51	2.7158	2.20706628	0.715987971	-102.3525207	123.0502239

T=350°C p=500psi N2

Exp #	PSOC	Wt. coal	Wt. FHC-470	THF-sol	THF-insol	daf	THFext	Yield sol%	Yield insol%
D77	1488	2.5115	4.926	5.687	2.0922	2.320626	0.275356988	20.92724172	90.15670772
D78	1498	2.4988	4.898	6.01	2.2184	2.28415308	0.334699441	34.030143	97.12133654
D79	1501	2.4989	4.997	3.309	2.0964	2.33597172	0.392593522	-89.06758178	89.74423714
D80	1504	2.5072	4.73	5.841	2.1546	2.29559232	0.381386219	31.78324718	93.85812896
D81	1448	2.4992	5.009	5.593	2.0517	2.19879616	0.450203514	6.084988171	93.31015022

T=400°C p=500psi N2							
Exp #	PSOC	Wt. coal	Wt. FHC-470	THF-sol	THF-insol	daf	THFext
D82	1488	2.5036	4.988	6.043	1.7392	2.3133264	0.316395873
D83	1498	2.5041	5.186	5.954	1.883	2.28899781	0.423713203
D84	1501	2.5067	4.897	5.756	1.7458	2.34326316	0.617814736
D85	1504	2.507	4.924	6.007	1.6477	2.2954092	0.6164023
D86	1448	2.5147	5.25	2.8961	1.6906	2.21243306	0.66212431

T=450°C p=500psi N2							
Exp #	PSOC	Wt. coal	Wt. FHC-470	THF-sol	THF-insol	daf	THFext
D87	1488	2.5116	5.105	2.682	2.8961	2.3207184	0.197507107
D88	1498	2.4954	5.026	2.886	2.871	2.28104514	0.261962209
D89	1501	2.5111	4.992	2.8479	2.71	2.34737628	0.358334055
D90	1504	2.5072	4.967	2.97	2.7266	2.29559232	0.520588205
D91	1448	2.5066	5.118	3.291	2.8253	2.20530668	0.715417145

T=350°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt. FHC-571	THF-sol	THF-insol	daf	THFext
D95	1488	2.5072	5.943	7.1	1.9873	2.269016	0.27411541
D96	1498	2.5129	5.398	6.43	2.1482	2.25030195	0.285104803
D97	1501	2.503	5.209	5.962	2.1129	2.3398044	0.328007398
D98	1504	2.508	5.171	6.794	2.0773	2.2933152	0.358370106
D99	1448	2.5093	4.225	5.108	2.1356	2.19664122	0.469650635

T=400°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt. FHC-571	THF-sol	THF-insol	daf	THFext
D100	1488	2.5148	3.572	4.356	1.6561	2.275894	0.410462991
D101	1498	2.509	5.409	6.167	1.7498	2.2468095	0.389543675
D102	1501	2.51	3.325	4.084	1.6961	2.346348	0.6407325
D103	1504	2.5072	5.417	8.402	1.6448	2.29258368	0.568294584
D104	1448	2.5039	5.62	7.925	1.6708	2.19191406	0.69220383

T=450°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt.FHC-571	THF-sol	THF-insol	daf	THFext
J80	1488	2.5219	5.0117	2.523	2.8784	2.28307607	0.271535712
J79	1498	2.5098	5.28	3.514	2.6384	2.25103962	0.303089766
J78	1501	2.5261	5.552	4.62	2.1042	2.33537945	0.365367336
J77	1504	2.5109	4.702	3.521	2.8	2.2874299	0.41621498
J76	1448	2.525	5.522	3.31	2.4852	2.2076075	0.536315371

T=350°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt.FHC-470	THF-sol	THF-insol	daf	THFext
J84	1498	2.5157	6.0262	7.242	2.0335	2.25633133	0.285865695
J83	1501	2.5249	5.596	6.361	1.9562	2.33427005	0.327231561
J82	1504	2.5239	5.408	6.444	2.1256	2.2992729	0.359301099
J81	1448	2.513	5.863	7.05	2.1075	2.1971159	0.469752124

T=400°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt.FHC-470	THF-sol	THF-insol	daf	THFext
J85	1488	2.504	4.956	5.599	1.6584	2.332476	0.420667691
J86	1498	2.5013	5.358	6.042	1.8195	2.2986947	0.398533943
J87	1501	2.5013	5.054	5.532	1.7287	2.35997655	0.644454136
J88	1504	2.4992	5.777	6.256	1.7022	2.30076352	0.570332565
J89	1448	2.4998	5.3695	6.972	1.5906	2.20157386	0.695254383

T=450°C p=500psi H2							
Exp #	PSOC	Wt. coal	Wt.FHC-470	THF-sol	THF-insol	daf	THFext
J95	1488	2.5044	5.373	3.057	2.842	2.3453706	0.278944659
J96	1498	2.5061	5.038	2.785	2.9159	2.3081181	0.310775061
J93	1501	2.4991	4.939	3.058	2.5689	2.35790085	0.368890782
J92	1504	2.4997	6.459	4.078	2.7354	2.30122382	0.418724887
J91	1448	2.5013	5.618	3.801	2.6417	2.20289491	0.535170496

R E S I D S B L A N K S
FHC-571 p=500psi N2

Exp #	T, °C	Wt. resid	THF-sol	THF-insol
D41	350	5.387	5.85	0.003
D42	400	4.066	3.026	0.004
D43	450	5.223	4.142	0.1947

FHC-470 p=500psi N2

Exp #	T, °C	Wt. resid	THF-sol	THF-insol
D74	350	4.999	5.352	0.0033
D75	400	5.015	5.037	0.0006
D76	450	60271	3.435	1.0667

FHC-571 p=500psi H2

Exp #	T, °C	Wt. resid	THF-sol	THF-insol
D92	350	4.78	5.338	0.0047
D93	400	4.906	5.526	0.0057
D94	450	5.276	4.634	0.139

FHC-470 p=500psi H2

Exp #	T, °C	Wt. resid	THF-sol	THF-insol
J90	400	6.291	6.335	0.0095
J94	450	4.782	2.853	0.6613

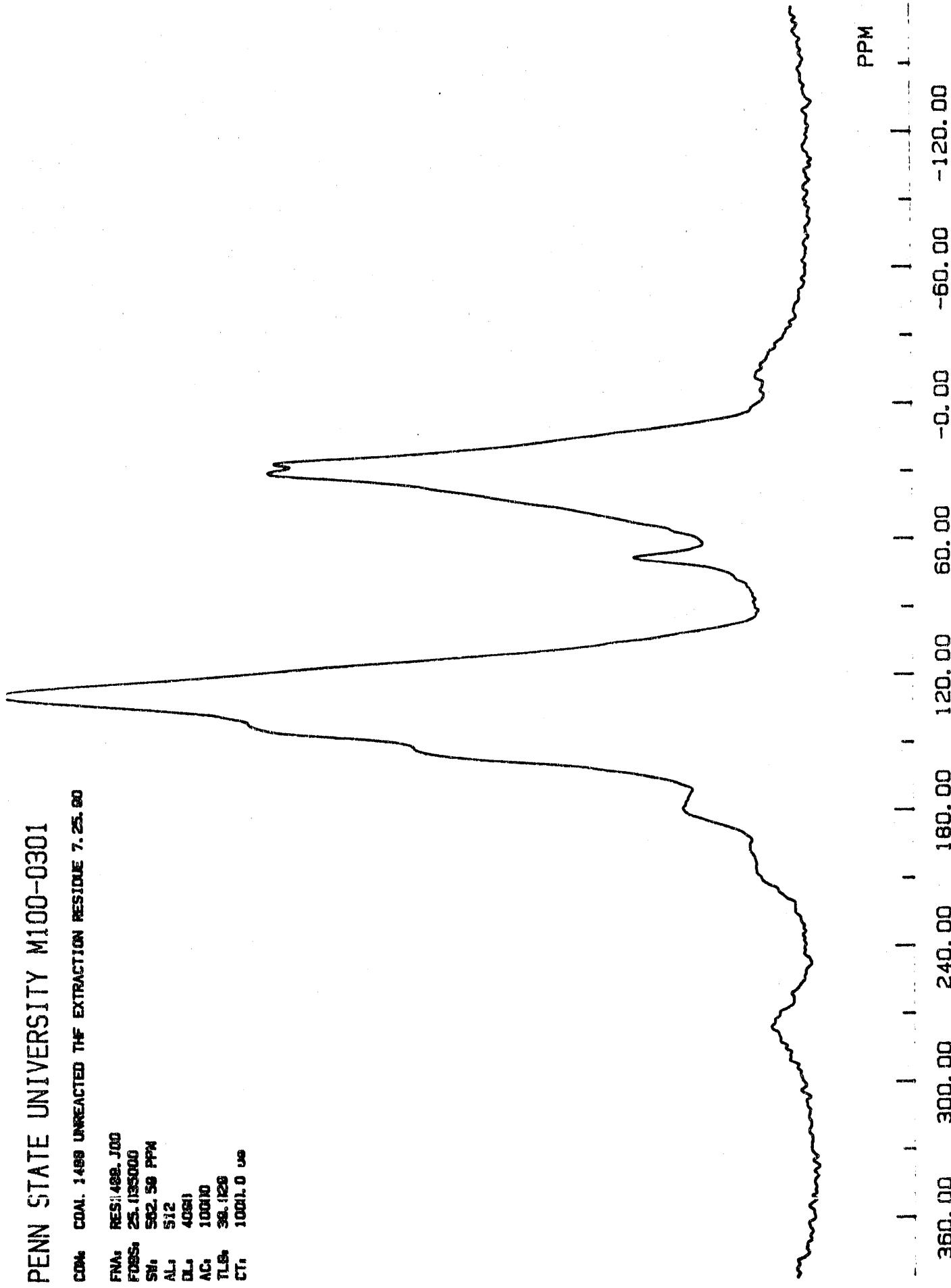
APPENDIX 3.

This appendix contains ^{13}C NMR spectra of a number of solid residues.

PENN STATE UNIVERSITY M100-0301

CORR. COAL. 1489 UNREACTED THF EXTRACTION RESIDUE 7.25.80

FNS₂ RES%489, JG0
FD35₃ 25.135000
Si₁ 502.59 PPM
Al₁ 51.12
D₁ 4051
AC₁ 10010
Tl₂ 38.126
CT₁ 10011.0 us



PENN STATE UNIVERSITY M100-0301

CDM: PSOC1488 N2 350 THF EXTRACTED CPMAS 7.10.90.

FNA: N21488.JD1

FOBS: 25.035000
SW: 562.59 PPM

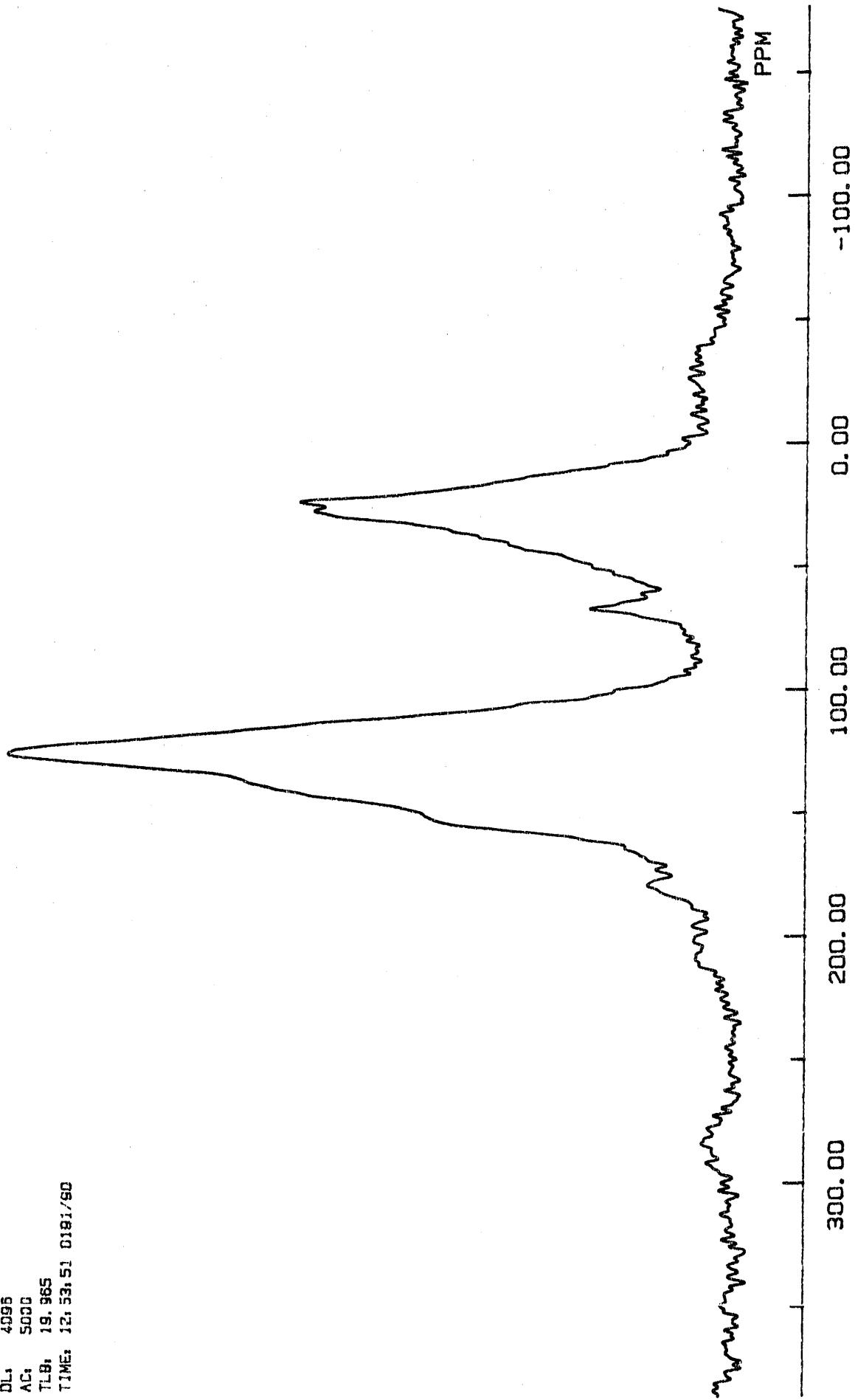
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AC: 5000

TLB: 19.965

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PENN STATE UNIVERSITY M1000-0301

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FNU EXP031.100

FD8S, 25.035000

SW, 562.59 PPM

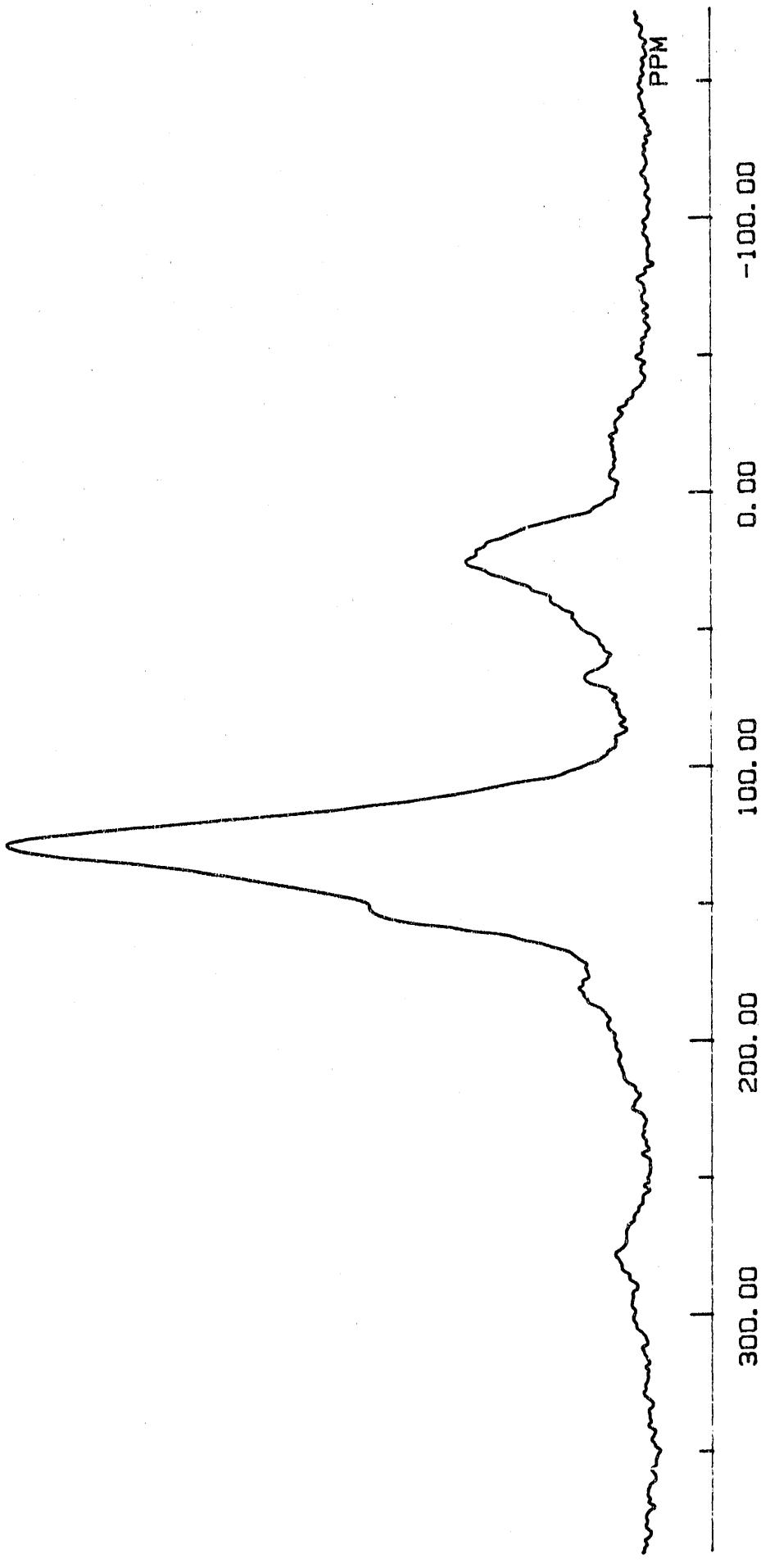
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AC, 10000

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PENN STATE UNIVERSITY M100-0301

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FOBS: 25. 035000

SW: 562. 58 PPM

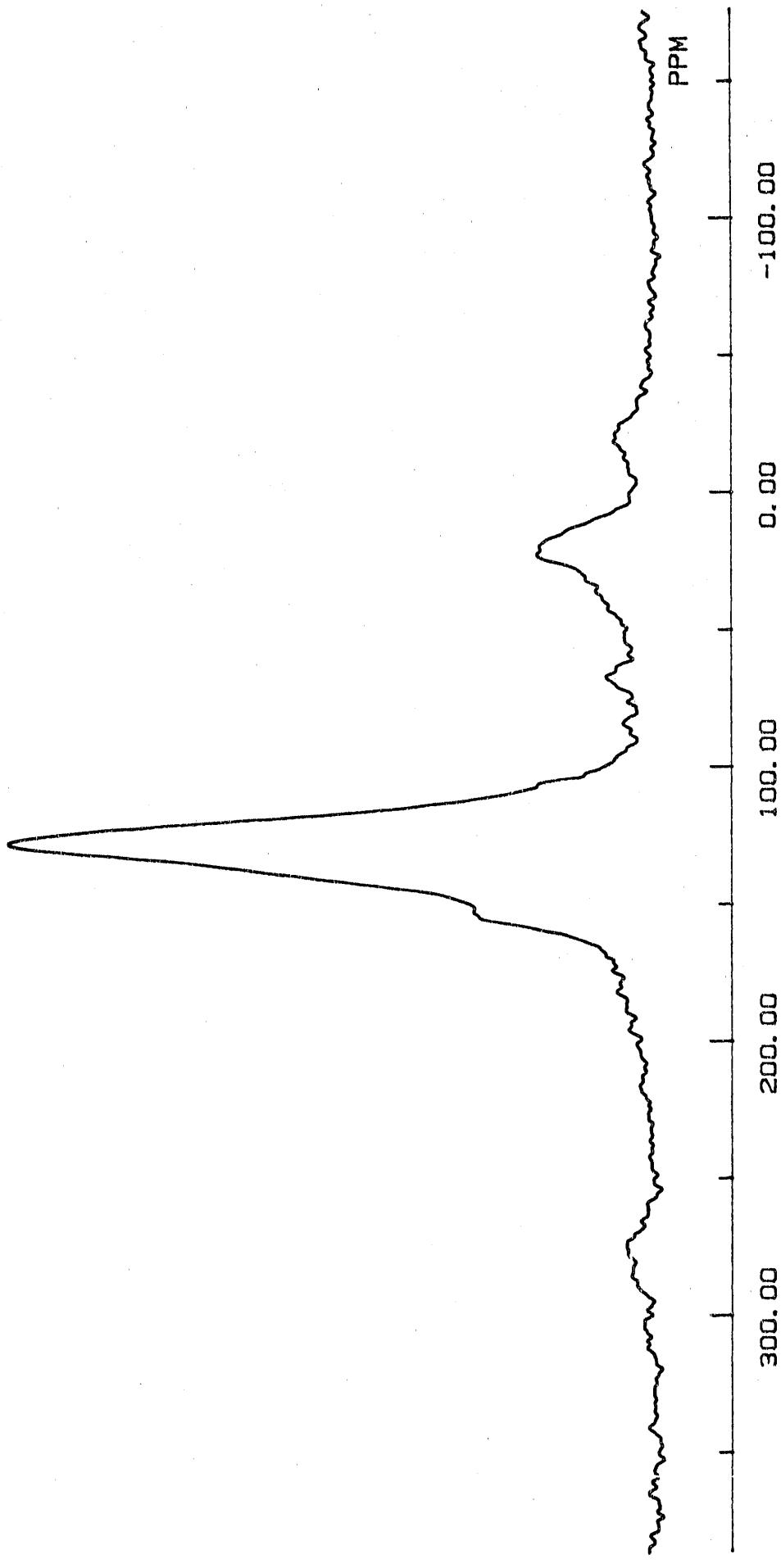
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AC: 100000

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PENN STATE UNIVERSITY M1000-0301

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FOBS: 25, 035000

SW: 512.58 PPM

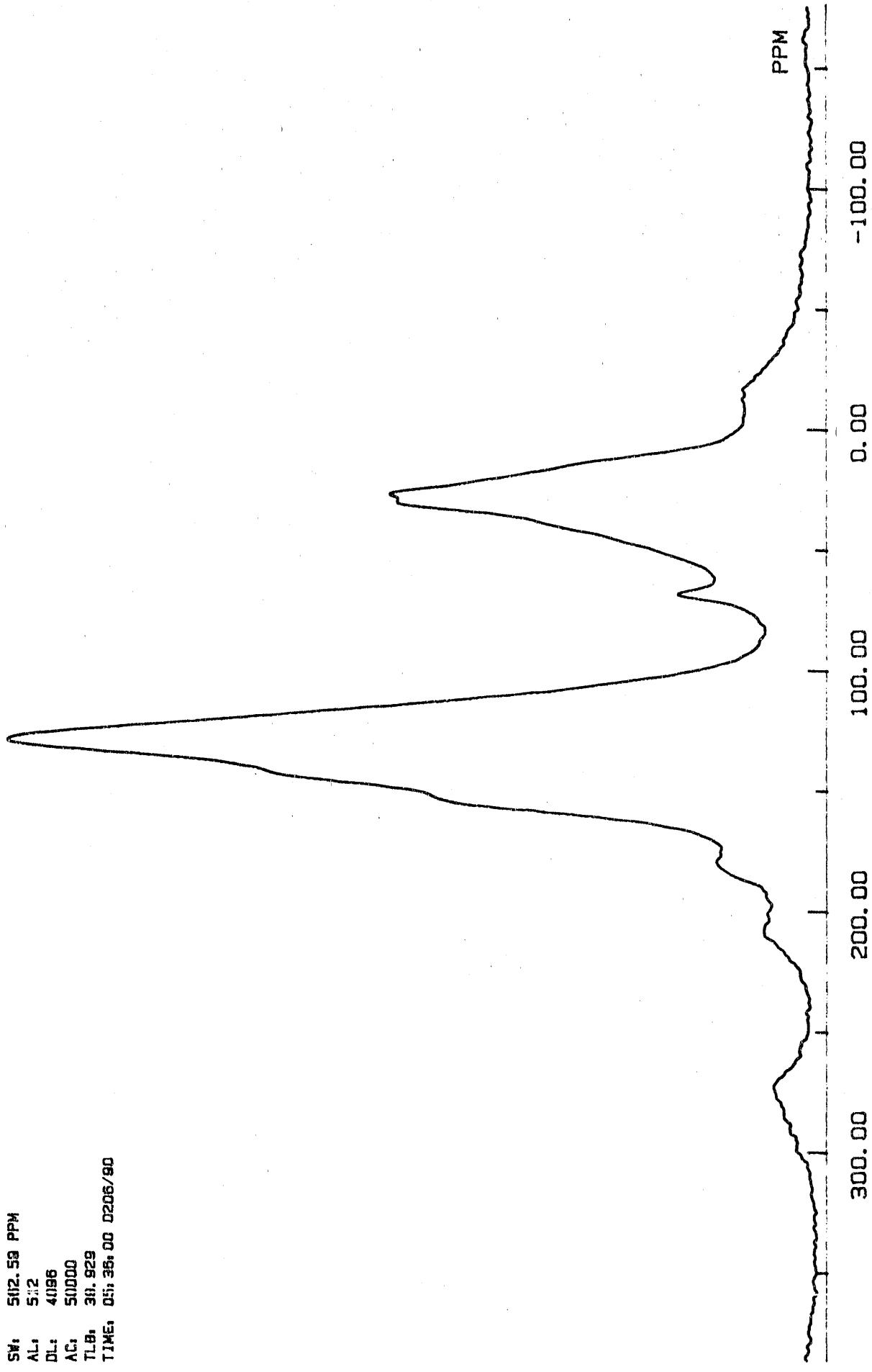
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AC: 50000

TLB: 38, 929

TIME: 05, 35, 00 0206/80



F
N
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DATE FILMED

11 / 29 / 90

