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Assessment of Treated Vs. Untreated Oil Spills

Final Report

February 1981

Prepared for:
U.S. Department of Energy
Assistant Secretary for Environment
Environmental and Safety Engineering Division

Under Contract No.: EY-76-S-02-4047 2502-768204047

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Washington, D.C. 20585

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16. Abstract This report describes the results of a series of studies conducted to determine the practicability and feasibility of using dispersants to mitigate the impact of an oil spill on the environment. The method of approach is holistic in that it combines the physical, chemical, microbial and macro-fauna response to a spill treated with dispersants and compares this with spills that are left untreated. The program integrates mathematical, laboratory, meso-scale (three 20 foot high by three feet in diameter tanks, described in Section 1), <u>in-situ</u> experiments and analyses to determine if the use of dispersants is an effective oil spill control agent. In summary, it appears viable to use dispersants as determined on a case by case basis. The case for using dispersants has to be based on whether or not their use will mitigate the environmental impact of the spill. In the case of an open ocean spill that is being driven into a rich inter-tidal community, the use of dispersants could greatly reduce the environmental impact. Even in the highly productive George's Bank area at the height of the cod spawning season, the impact of the use of dispersants is well within the limits of natural variability when the threshold toxicity level is assumed to be as low as 100 ppb, a level which is often found in the open ocean. Thus, it appears that dispersants can and should be used when it is evident that their use will mitigate the impacts of the spill. Their use in areas where there is poor circulation and therefore little possibility of rapid dilution is more questionable and should be a subject of future studies.			
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Preface

This study was undertaken over a period of four and one-half years, carried out under Department of Energy Contract No. E(11-1) 4047, through the Environmental and Safety Engineering under the direction of Dr. William E. Mott and Dr. John Cece.

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Last but far from least, is the office staff who enabled this rather voluminous to come to fruition in the form of a report. A special thanks to Ms. Corinne Carr who supervised the construction of the report and editing. Her patience, organization skills and thoroughness added greatly to reduce the difficulty of the formidable job of collecting and organizing the sections of this report. Other office staff who contributed much to this report are Ms. Tracy Miller who painstakingly did many of the flow charts and Denise Klein. Many thanks to the College of Engineering Word Processing personnel and especially to Mary Costa who did the bulk of the typing.

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EXECUTIVE SUMMARY

ASSESSMENT OF TREATED VERSUS UNTREATED OIL SPILLS

Mason P. Wilson, Jr.
Program Director

Executive Summary and Results

This report describes the results of a series of studies conducted to determine the practicability and feasibility of using dispersants to mitigate the impact of an oil spill on the environment. The method of approach is holistic in that it combines the physical, chemical, microbial and macro-fauna response to a spill treated with dispersants and compares this with spills that are left untreated. The program integrates mathematical, laboratory, meso-scale (three 20 foot high by three feet in diameter tanks, described in Section 1), in-situ experiments and analyses to determine if the use of dispersants is an effective oil spill control agent.

A series of physical and physical-chemical studies and experiments were conducted to determine the emulsification properties, including emulsion stability of the treated and untreated oil, and its rate of evaporation. Various natural entrainment processes were also investigated to compare natural entrainment of the oil with chemically dispersed oil. Emulsified oil exhibits properties in between those of a true solution and a suspension of immiscible phases. Experiments to typify the drop size distribution, mixing energy and to evaluate the effect that dispersants have on interfacial tension were conducted. The results of these tests indicated that only a fraction of the energy goes into the formation of droplets. Typical drop sizes were in the range of 2 to 10 microns for both the treated and untreated dispersed oil. This is well within the particle size range in which emulsions are classified, i.e., 0.25 to 25 microns, whereas butterfat particles are in the 7.5 to 8.5 micron range. The major difference between the dispersed oil and the chemically treated dispersed oil was not the drop size distribution but rather the concentration of oil in the dispersed phase. The amount of oil in the dispersed phase (hold-up) was approximately two to three times greater than the untreated dispersed oil for these tests. Consequently, the interfacial area of the treated dispersed oil was approximately two to three times greater. Entrainment was also observed without mechanical energy input with Corexit 9527, although the hold-up was slightly less than with mixing. As much as 86% of the oil that could be accounted for went into the water column when dispersants were used. A rather small amount of dispersant is required to decrease the interfacial tension (see Section 1).

The stability of the dispersed oil was investigated in several experiments, some of which produced conflicting results. The stability of an oil-in-water emulsion can be easily determined by measuring its settling or creaming rate. Most of the droplets follow a Stokesian flow. In the drop size range experimentally determined, it would take from 40 hours to 1000 hours (1 to 10 micron size) for the droplets to rise to the surface of a 0.6 meter tank. The amount of oil in the water column after twenty four hours of quiescent conditions remained relatively constant, however, the amount of oil in the water column when dispersants were used with mixing remained approximately twice that when no dispersants were used. In two separate tests, one with no mixing, the amount of entrained oil remained relatively constant. However, in these experiments chemical analysis of the dispersed phase indicated a ratio of dispersant to oil of approximately one to one. In Section 4.4, the experiment with no mixing is reported, and similar results were

found in the latest meso-scale tests reported in Section 8. Somewhat unusual results in terms of stability were also observed in the wind/wave experiments to be discussed in a later paragraph. Coalescence of the dispersed phase was found to be negligible (Section 1) and therefore did not affect the stability characteristics of the emulsion. It was found that very little agitation was required to maintain the chemically dispersed oil in the water column, (Section 4), however, it should be noted that in these tests the ratio of dispersant to oil in the water column was approximately one to one, even though application was on a twenty to one ratio. It should be noted, also, that these low ratios of dispersant to oil were only observed under quiescent conditions or when there was very little mixing energy applied. The mixing experiments had shown that almost all of the oil could be incorporated in the dispersed phase when mixing energy was applied and subsurface circulation was sufficient to maintain the dispersed oil from reforming at the water/air interface. It thus appears that more stable emulsions are formed when the dispersant/oil ratio is in the neighborhood of unity, however, natural turbulence and subsurface circulation in many instances could be sufficient to maintain almost complete entrainment of the dispersed oil.

The subsurface circulation and entrainment was investigated analytically and conditions for various drop sizes to remain in suspension were established. These results are presented in Section 4 of this report.

Several evaporation tests from an oil slick were conducted throughout the duration of this project and reported in Section 4, Section 7 and Section 12.2. In Section 7, laboratory and meso-scale tank evaporation tests are reported. The laboratory study using the self mixing dispersant Corexit 9527 indicated that the evaporation of the n-alkanes from the treated and untreated slicks were similar when the water was not agitated. However, when mixing was applied, the evaporation of the light n-alkanes, n-C₇ to n-C₁₀, from the treated slick were slower than from the untreated slick. The greater the mixing the greater the effect the dispersant had on depressing the evaporation rate. The dispersant affected the evaporation rate of the lighter n-alkanes to a greater extent than the heavier ones. The slower evaporation of the treated slick could be due to the mixing of some of the oil in the water column. Results of the meso-scale experiments were in agreement with the laboratory scale experiments when mixing was not applied. Evaporation was faster in the meso-scale (open tank) experiments because of the wind and more natural environment although mixing had little effect on decreasing the evaporation rates. Experimental results with treated and untreated oil showed that components lighter than C₁₂ evaporated from both slicks after three hours and after seventy-two hours all of the components up to C₁₆ had disappeared. The effect various wind speeds had on evaporation rates of Kuwait crude were investigated by using a wind tunnel. These results show that approximately 75 percent of the total evaporation occurs within the first two hours and that evaporation essentially ceases after twenty four hours with a weight loss of 32.3 percent. These results are in substantive agreement with the results reported in the preceding paragraph. Thus, if dispersants are applied two hours after the spill, most of the lighter weight hydrocarbons would have evaporated; furthermore, when dispersants are applied to the outer edges of the spill, it is being applied generally to the portion of oil

that has undergone the maximum amount of evaporation. Thus, the major portion of the more volatile and toxic fractions of the oil could be expected to be evaporated by the time dispersants would or could be applied in most situations.

Natural entrainment experiments were conducted in the wind/wave tank and in the rain drop experiment. Tests in the wind/wave experiments described in Section 3 of this report were conducted with fresh water and sea water with Kuwait crude. It was found that the oil weathers much differently in the fresh water than in natural sea water. In fresh water, it rapidly forms slicklets which appear to be stable emulsions and very little oil gets into the water column. In the salt water tests much more oil entered the water column and increased with time, except at a higher frequency where after weathering for 24 hours, the concentration of oil in the water column showed a dramatic decrease. This is attributed to the formation of stable emulsions that had an affinity to the droplets which took them out of solution. The appearance of the oil in the higher wave frequency tests showed a stringiness as though it had been shredded or torn apart after 24 hours. This did not happen with the lower frequency waves during the same period where the concentration increased with time in all salt water tests. The effect of an increase in temperature is to increase the amount of oil getting into the water column. Doubling the quantity of oil in the slick did not change the percent concentration of oil in the water column. Therefore, the actual concentration almost doubled. In the ocean, currents would carry some of the oil from under the slick. Tests using the dispersant did not show sudden increase in concentration of the oil in the water column immediately after adding the dispersant as might be expected. The visual properties of the slick and the waves changed, but the oil did not disperse into the water column until it had weathered over eight hours after adding the dispersant. After twenty-two hours of weathering, practically all the oil entered the water column.

Entrainment of oil into the water column by rain was investigated and reported in Section 4.4 of this report. The results indicate that substantial oil can be incorporated into the water column by this process. Concentrations as high as 45 parts per million were observed in these experiments, however, the concentration of oil in the water column drops off when either subsurface circulation or the rain is terminated. Consequently, natural entrainment by rain, like other entrainment phenomena, requires subsurface circulation to maintain the droplets in suspension.

A number of analytical chemistry techniques were developed throughout the duration of this project. These are reported in Sections 7, 9 and 12.2. Infra-red analysis of the petroleum hydrocarbons extracted from the water column were analyzed quantitatively as well as qualitatively. Several solvent systems were investigated in an attempt to separate the oil from the dispersant prior to infra-red analysis. Thin Layer and Column Chromatography were also used with various solvent systems to effect the separation; however, even with this system, a complete separation of the oil from the dispersant could not be realized. Because of this and of the time required to perform this separation, it was decided that development of computer techniques to effect spectral separation of these two components was required. This technique is

reported in Section 12.5.

A quantitative analytical infrared technique to determine the ratio of dispersant to oil was also developed and is reported in Section 12.2 of this report. It involves the ratio of absorbance of the mixture at a wave number of 3600 (cm^{-1}) which corresponds to the OH stretching. This represents a strong peak for most dispersants, while the peak for most oils occurs at a wave number of 2930 (CH stretching). Mixtures were prepared to establish calibration curves and a procedure was developed to determine the ratio of dispersant to oil in the mixture and the total amount of hydrocarbons present in the sample. In Section 8, a quantitative gas chromatograph method is described that determines the total peak area of Corexit 9527 in the water stock solutions. This area was converted to concentration of oil and subtracted from the integrated total hydrocarbon in the oil-dispersant mixture. This gave ratios of oil to dispersants almost identical to those determined by the infra-red method mentioned above. A GC Mass Spectrum system was also used in portions of the analysis as reported in Section 7 of this report.

The chemistry of the treated and untreated oil slick was investigated rather extensively and is reported in Section 7 of this report. Some of these results were discussed in the preceding paragraphs on evaporation and entrainment. Most of the chemical analyses were conducted on tests run in the meso-scale tanks. These tests were run in the tanks under the following conditions (1) batch, with no mixing or forced circulation (2) batch with mixing provided by the wave maker and (3) with dilution (flow-through) and mixing. Salt water from Narragansett Bay was used as the test medium and the salt water temperature was maintained to within 1°F of the Bay temperature to eliminate any thermal stresses on marine organisms that were present. One series of tests were conducted to determine the effect of various modes of application of oil and dispersant to the seawater on the concentration of oil in the water column. It was found that the effectiveness of the dispersant in carrying the oil into the water column is proportional to the amount of contact of the dispersant with both the polar water fraction and the non-polar fraction of the oil/water system. The most intimate contact between these fractions was achieved when the dispersant was premixed with the oil. In all experiments, agitation of the water surface in the tanks also aided in mixing the oil/dispersant complex into the water column. Controls were used throughout the duration of these tests and remained within the hydrocarbon levels found in the Bay. In the dispersant treated tank, the highest concentrations were found generally in the top and middle layers after one hour, with a relative reduction in concentration after twenty-four hours (in some cases reduction to control levels). The level of hydrocarbons was determined more by the mode of application than by the amount of oil/dispersant added. In the untreated tank the oil concentration increased initially but often fell below control levels after twenty-four hours. The cause for this behavior is not fully understood but it is believed that the oil droplets suspended in the water column combine with the surface slick and do not get re-entrained.

Analysis of sediments in flow-through experiments had indicated no significant increase in concentrations of petroleum hydrocarbons over a three week period for either the treated or untreated surface slicks.

Microbiological studies were conducted throughout the program in order to determine whether the degradative capacity of the petroleum hydrocarbons and natural microorganisms were enhanced by the use of dispersants. It was determined that the Viable Plate Count (VPC) and Most Probable Number (MPN) methods were suitable for enumeration of marine heterotrophic bacteria and hydrocarbonoclastic bacteria. Use of these methods demonstrated that the percentage of oil degraders within the "total heterotrophic population" increased with exposure time of the "total population" to oil and/or dispersant.

Oxygen depletion by the Modified Biological Oxygen Demand method is a valuable tool which provides a general picture of biological response to materials suspended in the water column. The procedure was used to demonstrate the biodegradable nature of Corexit 9527 and provide a rough index of degradation potential. This method confirmed VPC and chemistry data in the meso-scale experiments.

Oxygen depletion has certain limitations, the greatest being that it cannot be directly correlated with actual oil degradation rate or the rate of degradation of specific oil components. An alternate approach is chemical analysis by gas chromatography which has been used in this project. The use of this technique for water column samples, while quantitative for bulk oil, has certain limitations for component analysis. It is possible to demonstrate loss of classes of compounds by this method but is too expensive and time consuming for routine degradative rate determinations. The use of ^{14}C labeled hydrocarbons allows a fairly simple method for measuring mineralization (conversion of organic carbon to carbon dioxide by metabolism) as an index of biodegradation. Representative hydrocarbons provide an estimate for the rate at which the mixed natural population achieve mineralization of aliphatic and aromatic hydrocarbons. The mineralization rate studies demonstrate turnover rates ranging from approximately 20 to 90 mg of substrate per hour. These values compare with results by other investigations in similar systems.

A more accurate approach using ^{14}C methodology is to measure not only mineralization, but also the production of water soluble intermediates which carry the ^{14}C label and the amount of ^{14}C incorporated into cell biomass. The importance of this approach was apparent in one typical experiment as discussed in Section 8 of this report.

Studies by the VPC for the surface film, water column and sediment were performed at 13 and 4°C. The bacterial numbers increased in the surface film during day 1 and 2 then remained essentially constant throughout the 21 day experiment. We interpret this increase not as bacterial growth per se but rather the formation of the microlayer. The sediment bacterial population increased through a period of nine days in the control, dispersant and oil-dispersant trials but not in the oil tank. The numbers remained constant in the sediment of the oil-dispersant tanks following these nine days but declined in the control and dispersant tanks. It is believed that the hydrocarbon degrading bacteria are carried into the oil film in the oil treated tank, removing them from an active role at the oil water interface. This might be expected because the oil destroys the surface microlayer.

The water column studies at 4^o and 13^oC provide evidence for two different bacterial populations in the natural seawater which was at 1^oC. The total heterotrophic population shifts somewhat but the most significant observation is a rapid increase in the number of hydrocarbonoclastic bacteria through day 7 followed by a decline to original numbers due, we conclude, to exhaustion of the nitrogen, phosphorus and iron centers of the seawater.

The studies showed a decline in colony diversity with time in the tank system suggesting enrichment for specific organisms which is supported by the studies on the ratio of hydrocarbonoclastic to heterotrophic bacteria. Population dominance is more significant than population size which is a fairly constant value.

The long term flow through experiment showed no significant correlation between the number of total heterotrophic bacteria and hydrocarbon concentration, but a significant correlation was found between total heterotrophic and total hydrocarbonoclastic bacteria which indicated selection for hydrocarbon-utilizing bacteria.

A negative relationship was found between hydrocarbon content and hexadecane or naphthalene mineralization rates, suggesting inhibition of mineralization at high hydrocarbon and/or dispersant values. However, there was a decrease in hydrocarbon turnover time in the oil and/or dispersant tanks. This decrease in the turnover time is more apparent for aliphatic hydrocarbons than for aromatic hydrocarbons.

The variation in mineralization rates is minimal ranging from 8.6 to 11.9 ng/hr for hexadecane and 8.3 to 19.6 ng/hr for naphthalene. Thus, in the determination of degradation time the most important function is hydrocarbon concentration.

Investigation of phosphate and nitrogen in the test systems reveal values which were always nutrient limiting for the amount of degradable carbon available.

It is our conclusion that hydrocarbon degradation potential in nutrient limited seawater is a relatively constant value independent of the presence or absence of oil in the water column. There is selection for hydrocarbonoclastic bacteria with time but their overall degradation activity as a mixed population is not significantly affected by the enrichment process. Preliminary evidence indicates that nutrient supplements (nitrogen, phosphorus and iron) do have a significant effect on the size of the seawater microbial population and yield a rather homogenous population of hydrocarbon utilizing bacteria in the presence of oil.

A brief discussion of nutrient seeding suggests this is not a viable approach to increased hydrocarbon degradation potential. The danger of increased pathogenicity in nutrient enriched oil-water systems is a real possibility which must be more fully investigated.

Natural microbial hydrocarbon degradative processes are active in the water column of dispersed or non-dispersed oil. These processes

will eventually lead to the turnover of the biodegradable oil components. The rate at which oil degradation occurs is not materially enhanced by the dispersion process but dispersion of the oil into small micelles (1-2 μ) suspended in the water column does make the oil more available to microbial action. Due to the physical inaccessibility of microorganisms to the bulk of the oil in a heavy slick, dispersion of the oil is an adjunct to the hydrocarbon degradative capacity of a mixed natural marine water column population.

This project has not shed much light on the affect of microbial populations on dispersed oil entrained into sediments or oil solubilized or suspended as sub-micron micelles in surface microlayers. Limited data from this project indicates that hydrocarbon degradative potentials in sediments and the surface microlayer may be significantly higher than degradative potentials in the water column.

An investigation into the effects of realistic concentrations of oil and oil-dispersant mixtures on marine life was conducted. The results are reported in Section 9 of this report. The investigation of short term exposure of bay scallops, Argopecten irradians, and two scallop predators, the oyster drill Urosalpinx cinera and the common starfish Asterias forbesi, to oil and oil-dispersant mixtures suggested that predator and prey have different lethal susceptibilities. Scallops were most sensitive to dispersant and dispersant mixed with oil, starfish were only sensitive to the dispersant while the oyster drill seemed unaffected even though all were exposed to dilutions of identically prepared stock solutions. Scallops were least susceptible during winter months and most susceptible at summer temperatures. Treatment had less effect on predators than on scallops at summer temperatures. Sublethal concentrations of dispersant and oil-dispersant mixtures diminished the behavioral ability of scallops to recognize drills and starfish. The degree of effect increased with temperature. Predator detection of prey at the same concentrations was more complex. The feeding response, or posturing reflex of starfish was significantly slowed by all treatments. In contrast, drills were unaffected in their recognition of scallop effluent in a choice chamber after treatment. The results indicate that scallop populations may suffer more than the direct impact of a pollutant which selectively affects scallops but not all of the scallop predators. The differential susceptibilities of the various species investigated in this study points out a problem biologists face when conducting and interpreting a bioassay. Because not all animals are affected by the same chemicals at the same concentrations and that animals have ecological relationships which should be considered, indicates that knowing the response of one species to a number of pollutants is not always sufficient for ecological assessment.

In light of the differential susceptibilities demonstrated in the simple three animal system investigated, the concept of an indicator species is difficult to defend. It would seem that because each organism can have its own array of chemical compound and concentration response, there is no logical reason to assume that one animal could possibly be used to accurately judge susceptibility arrays for other species.

In order to have conducted the above reported study, it was necessary to study the behavioral recognition of the scallop to its predators. It was necessary to develop a method for quantifying the scallop's response to prey. This resulted in defining a "clap index" which is a measure of the scallop's escape response. This study is reported in Section 9.2 of this report. Field and laboratory studies of the intensity of predation by the oyster drill on the bay scallops are reported in Section 9.3 of this report.

The investigation of community type responses discussed above suggested that sublethal concentrations of dispersants had adverse effects on scallop behavioral escape responses and starfish posturing reflexes. These results led to the construction of a simple community to determine what would happen if both predator and prey were dosed and placed together in large laboratory tanks. How many scallops would survive each treatment? Is it possible to detect changes in individual spacing with treatment? The purpose of the experiment was to determine the answer to these questions. The results of this study show that when both predator and prey were treated as a community, scallop survivorship was significantly reduced in the dispersant and oil-dispersant mixtures beyond that expected because of hydrocarbon treatment or starfish predation alone. Since scallop survivorship in the oil treated tank was not different from the control, the slowed ability of the starfish to respond to food did not appear to affect their ability to feed on scallops. The results of this experiment show that at concentrations far below the LD₅₀, dispersant treated scallops suffer greater than 50 percent mortality in the presence of starfish. Chemical analysis of the scallops at the end of this experiment showed that there was no significant increase of petroleum hydrocarbons in scallops as compared to the control. These results are not predicted by the classical bioassay methods. Community studies are rare to non-existent in bioassay work but could prove extremely useful in the prediction of ecological impacts by dispersants.

The validity of the results of any environmental research program rests on its ability to be applied to the real environment. This program is no exception; consequently, in the formative stages, it was decided to respond to spills of opportunity to determine the validity of the bench scale and meso-scale tests. This portion of the program has proved to be very beneficial, and has validated a number of the results that were obtained throughout the various phases of the program. The team responded to three spills of opportunity.

The first of these spills was the Argo Merchant in 1976, the largest recorded spill in U.S. history. This first spill of opportunity served as a proving ground to field test the techniques developed in the laboratory. A portion of this work was reported in the Interim report of April 1977, and in a host of other places, included the proceedings of the Argo Merchant Symposium held at the University of Rhode Island in January 1978.

The second spill of opportunity occurred late in January 1977 in the ice-choked Buzzards Bay at the entrance to the Cape Cod Canal. This spill of No. 2 fuel oil, the result of a grounding of a barge, gave us

another opportunity to test our developments under a series of circumstances quite different from those of the Argo Merchant. The material spilled, a No. 2 fuel as compared to a No. 6 for the Argo Merchant, and extreme icing posed many new problems to be solved. Sampling under these conditions more resembled a response to a spill in the Arctic than what would normally be expected to occur in the North Atlantic. Both of these spills served to confirm the experimental results that were being obtained in the laboratory. Very early in the feasibility study, attempts were made to mimic a spill in a natural environment. Under the simulated natural environment tests, it was found that very little of the oil was getting into the water column, far less than is normally used for bioassay and LD₅₀ type tests. These results were also confirmed in the field by other investigators. The Buzzards Bay spill also provided air, surface, and water column samples at the spill site. A sample of oil was obtained from the barge and exposed in the laboratory under simulated conditions. The resulting chromatograms of these laboratory tests were almost identical to those found in the field. To our knowledge, this was the first time that a complete set of air, surface, and water column samples taken in the field were duplicated in the laboratory. Furthermore, it confirmed that the lighter fractions, i.e., C₁₀-C₁₂ and below, enter the atmosphere in the field. This leads one to question the validity of many toxicity tests where these components were not allowed to evaporate and were forced into the water column. This work has been continued in the laboratory and the meso-scale tanks, with and without the use of dispersants, during this second year of the contract. This work confirms the validity of the approach that was instituted in the early phases of this project. The major result of this additional work shows that the effect of the use of dispersants is to delay the evaporation of the lighter components by as much as 24 hours in the laboratory; however, they eventually evaporate. These results are essentially duplicated in the meso-scale tests; however, on a much more compressed time scale. This compression of the time scale in the meso-scale tests, which more closely approximates the field, is very significant. Processes that require 24 hours to occur in the laboratory occur in approximately two hours in the meso-scale tanks. Evaporation is enhanced in the meso-scale tests because of their exposure to a more natural wind and atmospheric environment.

Chemical analysis of the water column in these tests also shows some interesting results. Oil concentrations in the water column of the untreated tanks never exceeded 0.8 ppm, and very rapidly would return to the control values. The general trend when dispersants are used is that the oil concentration approaches the control value after 72 hours at most levels in the tank. The chromatograms of these water column samples also support the evaporation results mentioned above, which show that very little of the lighter fractions (below C₁₂ - C₁₄) remain in the water column.

The third spill of opportunity to which this team responded was the September 21, 1978 West Hackberry, Louisiana, incident.

During the recent West Hackberry #6 cavern decompression accident, an estimated 72,000 barrels of oil were released. Of this amount, an estimated 52,000 barrels of oil were recovered, and an estimated 20,000

barrels were burned or were unrecoverable from the diked area.

The University of Rhode Island (URI) project relating to the treatment of oil spills contains a task involving response to "spills of opportunity." Having participated in the Buzzards Bay and Argo Merchant incidents, the URI project team was easily assembled and rushed to the scene.

Upon arrival in West Hackberry, they were joined by Department of Energy (DOE) personnel and representatives from Dames & Moore (Houston Office) and the University of New Orleans. This incident presented an opportunity to put into practice some of the "contingency plans" developed by these groups.

The Department of Energy (DOE) organized the assemblage into an Environmental Assessment Team whose objectives are to:

- determine the geographical area covered by the DOE effluent
- assess the environmental impact caused by the DOE effluent

To meet these objectives, an Environmental Assessment Plan was drafted and presented to the Regional Response Team (RRT) which had convened in West Hackberry. The RRT reviewed and accepted the plan.

Having established its procedures and sampling requirements, the team collected more than 500 scientific samples. The sampling was conducted in affected as well as unaffected areas of water, marsh, and terrain. The samples were appropriately preserved, indexed, catalogued, and rank ordered into priority categories. The high priority samples were analyzed for the presence of oil, generally, and DOE oil, specifically.

Based upon the results of these analyses the team returned to West Hackberry at approximately 3, 6, and 12 months after the incident. The re-visits and selected re-sampling will assist in documenting the overall affect of the incident. The results of this investigation are reported in a separate report.

As part of the project for assessing the environmental impact of treated versus untreated oil spills, a fates model was developed which tracks the surface and subsurface oil. The approach used to spread, drift and evaporate the surface slick is similar to that in most other oil spill models. The subsurface technique, however, makes use of a modified particle-in-cell method which diffuses and advects individual oil-dispersant droplets representative of a large number of similar droplets. This scheme predicts the time dependent oil concentration distribution in the water column which can then be employed as impact to a fisheries population model to be discussed later. In addition to determining the fate of the untreated spill, the model also allows for chemical treatment and/or mechanical clean-up of the spilled oil. With this capability, the effectiveness of different oil spill control and removal strategies could be quantified.

The model was applied to simulate a 34,840 metric ton spill of a No. 2 type oil on Georges Bank. The concentration of oil in the water column and the surface slick trajectory were predicted as a function of time for chemically treated spills occurring in April and December. In each of these cases, the impact on the cod fishery was determined.

The important distinguishing feature between a wind driven surface slick and a chemically treated slick is that in the treated slick the oil enters the water column directly beneath the slick and is subject solely to local advective currents and diffusion. The wind driven surface slick can be beached in the intertidal zones, estuaries and marshes which are highly productive, while the treated oil remains in the water column. Various cases were studied in this modeling behavior and concentration profiles were calculated over a period of a thirty day simulation of a 34,840 metric ton oil spill at a time when the cod were at their spawning peak. Experimentally determined subsurface currents were used, as well as, average wind data collected for the area for the time of year the spill was assumed to occur. The analysis shows the divergence of the trajectories of the treated and untreated spills. The results of these simulations are presented in Section 5 of this report.

A fisheries-oil spill interaction model was developed to estimate first order effects of the impact of a treated versus an untreated oil spill on the commercial fish catch over ensuing years. The primary effect is assumed to occur through egg and larval mortality. The biological model formulated contains as subcomponents; a population model of the fishery, a model for advection and diffusion of oil, and fish larvae, and is coupled to the oil behavior and fates model described previously.

A two day 34,840 metric ton oil spill occurring on December 15 was simulated and a sensitivity analysis using the fisheries model was conducted. Impact predictions were conducted under three theoretically acceptable piecewise-smooth larval mortality curves, three threshold toxicity values of 1,000 and 50,000 parts per billion (ppb) and three application scenarios in which 0%, 50% and 100% of the oil is chemically treated.

Decreasing impact is associated with increasing larval resistance to oil toxicity (increasing threshold values), with decreasing entrainment and with increasing mortality modes (three different natural mortality modes were used). For a given treatment scenario and toxicity threshold, although the same number of eggs and larvae are lost from the system due to the spill, the effect of different natural mortality modes can show quite different results.

One of the most significant findings was that the natural mortality regime for the population was more important than either threshold toxicity values or the percent of oil dispersed in the water column. The importance of determining appropriate mortality regimes and threshold values is manifested from the results. The results indicate that if an oil spill was driven towards the islands of Nantucket and Martha's Vineyard rather than out to sea, dispersants would be used with little cost to the fishery, using a toxicity threshold as low as 100 ppb. The results do show, however, that the use of dispersants have a greater

effect on the cod than the untreated case. This is not surprising since making the oil more available to local marine biota is expected to increase mortality. The principal decision for using dispersants has to be made on the basis of whether or not their use will prevent more significant damage if the spill is allowed to come ashore and into highly productive intertidal zones and marshland where the oil can be expected to remain over an extended period of time. The other consideration is the time response of the ecosystem. Will the ecosystem recover more quickly to its prespill state than if the oil is left untreated?

The magnitude of the impacts estimated in this study range from 0% to 10% of the annual maximum sustainable yield of approximately 25,000 metric tons or up to \$2.5 million in reduced income to the fishing fleet. Simulation of a 30 day oil well blowout shows impacts four times as large, so that the specific scenario is of considerable importance.

Another significant result of this simulated study is that even in the worst case, the expected mortality due to the spill is well within the limits of the observed natural variability of adult cod. This sheds some doubt on the use of an abundance of a particular species as a measure of the impact of a spill.

In Table I the results of this project are summarized. Inspection of this Table reveals that little evidence was found to support some common beliefs of the effects of the use of dispersants. For example, dispersants were expected to drive the lighter, more toxic components of the oil into the water column. In this study, it was found that this effect was insignificant. It was also expected that the use of dispersants would enhance biodegradation and it was found that the hydrocarbon degradation potential in nutrient limited seawater is a relatively constant value, independent of the presence or absence of oil in the water column. Expected results were that the use of dispersants increases mortality in the immediate vicinity of the spill but could mitigate a greater impact had it been allowed to reach the rich intertidal communities.

In summary, it appears viable to use dispersants as determined on a case by case basis. The case for using dispersants has to be based on whether or not their use will mitigate the environmental impact of the spill. In the case of an open ocean spill that is being driven into a rich inter-tidal community, the use of dispersants could greatly reduce the environmental impact. Even in the highly productive George's Bank area at the height of the cod spawning season, the impact of the use of dispersants is well within the limits of natural variability when the threshold toxicity level is assumed to be as low as 100 ppb, a level which is often found in the open ocean. Thus, it appears that dispersants can and should be used when it is evident that their use will mitigate the impact of the spill. Their use in areas where there is poor circulation and therefore little possibility of rapid dilution is more questionable and should be a subject of future studies.

TABLE I.

Summary of the Characteristics of
Treated versus Untreated Oil Spill.

Untreated Spill	Treated Spill
1) The 'drifting' and spreading oil slick continually moves over new water.	1) Since treating agents disperse oil into the water column, the dispersed oil moves with the water column as a direct result of currents and diffusion.
2) Microbial Utilization.	2) Hydrocarbon degradation potential in nutrient limited seawater is a relatively constant value independent of the presence or absence of oil in the water column. There is a selection for hydrocarbonoclastic bacteria with time but their overall degradative activity as a mixed population is not significantly affected by the enrichment process.
3) Suspended sediment transport and sediment contamination.	3) There was no evidence for increased sustained sediment contamination when dispersants were used.
4) Evaporation.	4) Treating agents caused slight delays in evaporation when compared with the untreated spill; however, the difference was not significant.
5) Dissolution and emulsification.	5) The use of dispersants does increase the amount of oil in the water column.
6) Toxicity and Subacute toxicity.	6) The use of dispersants increases the availability of oil to marine organisms and results in higher mortality in the immediate vicinity of the spill. Predator-prey relationships can be altered in such a way that mortality can be much greater than expected from acute toxicity considerations.
7) Impact on selected species.	7) A sensitivity analysis of a 34,840 metric ton spill at the height of spawning season estimated that the maximum expected impact would be 10% of the annual fish catch, well within the expected natural variability of this particular species.

LIST OF PUBLICATIONS AND PAPERS PRESENTED
OF THE U.R.I. OIL SPILL RESEARCH TEAM

1. "The Spreading, Retention and Cleanup of Oil Spills," University of Rhode Island, HCP/P2756-01-UC-11, NTIS.
2. "Assessment of Treated Versus Untreated Oil Spills (Interim Report)" University of Rhode Island, June 1978, HCP/W4047-02, NTIS.
3. "The Assessment Problems of Whether or Not to Treat Oil Spills," M.P. Wilson, Jr., Proceedings of the ASTM Symposium on Chemical Dispersants for the Control of Oil Spills, October 1977.
4. "Effect of a Chemical Dispersant on Microbial Utilization of Petroleum," R.W. Traxler and L. Bhattacharya, *ibid.*, University of Rhode Island.
5. "Chemical Analysis of Dispersed Oil in the Water Column," M. Ahmadjian and P.F. Lynch, *ibid.*, University of Rhode Island.
6. "Drop Size Distributions in a Treated Oil-Water System," W. Jasper, T.J. Kim, M.P. Wilson, Jr., *ibid.*, University of Rhode Island.
7. "Computerized Dispersive Infrared Spectroscopy," W. Jasper, T.J. Kim, M.P. Wilson, Jr., *ibid.*, University of Rhode Island.
8. "Application of an Oil Spill Computer Model to Narragansett Bay and Rhode Island Sound," C. Noll, M. Spaulding, Presented at IOPPE Conference in Hamburg, Germany, Sept. 1978.
9. "Collection and Analysis of Treated and Untreated Oil Spill Vapors," D. Goldfarb, M.S. Thesis, Department of Chemistry, University of Rhode Island, 1978.
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16. "Summary of Physical Studies," M.P. Wilson, Jr., *ibid.*, University of Rhode Island.
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1.0 Introduction, Background, and Program Description

Mason P. Wilson, Jr.

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Introduction, Background and Program Description

1. BACKGROUND

In 1976, the U.S. Office of Technology Assessment presented an interim report on the coastal effects of offshore oil and gas development (1). One of the factors stated in this report of concern to coastal states, involves basic uncertainties about environmental and economic impacts. Studies estimate that the total probable oil spills from offshore continental shelf operations ranges from a low of 85,000 barrels to a high of one million barrels and that one out of ten spills from a drilling or production platform would reach a beach in New Jersey or Delaware. Present United States policy for combating oil spills is concentrated on physical containment with mechanical or sorbent removal techniques. When these means fail, the uncontrolled, untreated spill can cause considerable damage to the marine environment, especially to birds, saltwater marshes and beaches, where marine life is most plentiful, and where the juvenile forms of many commercial fish have their origin. It is these juvenile forms that appear most susceptible to oil pollution. The use of treating agents for final clean-up and for preventing the spills from reaching the shore and mitigating the environmental impact, when mechanical means fail, has been minimal because of the lack of information concerning the use of these agents and their affect on the environment. Since the Torrey Canyon spill in 1969 off the coast of England, where dispersant use produced disastrous results, there has been considerable development of treating agents that are far less toxic than those available at that time. Furthermore, it has since been determined that it was not the dispersants that caused the extensive damage in this spill, but rather the toxic solvents in which the dispersants were dissolved. New dispersants either use non-toxic solvents or sea water for their solvent base.

The debate over whether to use dispersants to treat oil spills has been long and controversial. The truth about dispersants, their use and effectiveness has often been obscured by undocumented and, at times, emotional opinions. Certainly, the excessive use and unfortunate experience with dispersants on the Torrey Canyon spill serves to form the basis for most of the criticism. Additional criticism concerning the use of dispersants is grounded on the belief that even if the dispersants themselves were not toxic, the use of these agents make the oil more toxic by its increased dispersion within the environment (2). This viewpoint, however, is applicable only to the immediate vicinity of the spill. The principal question to be answered in the use of a dispersant, is, "will its use cause less environmental damage, even though there is increased toxicity in the vicinity of the spill, than the untreated spill?" Furthermore, will the environment recover more quickly when dispersants are used than the long term effects of an untreated spill such as reported by Blumer (3). These are extremely difficult questions to answer. However, one use of dispersants is based on the premise that if treated at sea, most of the damage in the intertidal zone and salt water marshes where there is a concentration of marine life, could be mitigated. It is well known that marine life is concentrated in three major areas: (a) the surface, (b) the benthic zone, and (c) the inter-tidal zone. It is these three major areas that

the uncontained, poorly dispersed oil spill is concentrated (4), whereas, the majority of oil in the chemically treated spill is concentrated in the water column where it is more easily diluted by tidal flushes and where there is less concentration of marine life. The affect of oil on the marine environment has long been a concern to the environmentalists and oil companies alike. The severity of biological damage depends on many factors, some of the major ones are: the type of oil spilled, the dose of oil, the physiography of the area, weather conditions, type of local biota, season, previous exposure of the area to oil and other pollutants and the treatment of the spill. Three conditions are especially critical, and some researchers claim that all three must exist simultaneously for a spill to have significant environmental damage. The conditions are:

- (1) The volume of oil spilled must be large with respect to the body of water being impacted.
- (2) The oil should be refined.
- (3) Storms or heavy surf must cause the spilled oil to be churned into bottom sediments (5).

Whether or not these conditions occur, some part of marine life is likely to be affected by an oil spill. Studies from more than one hundred major oil spills over a twelve year period indicate that birds are the type of marine life most often affected (6).

The use of dispersants to mitigate the impact of oil spills have been used almost exclusively in the United Kingdom where it appears to have had minimal impact on the environment. Caution should be exercised in transferring the United Kingdom results to the use of dispersants along the United States coastline. Britain has very high tides, especially in the Milford Haven area in Wales where dispersants have been extensively used. The tides in this area range from twenty-four to twenty-eight feet. An example of the use of dispersants to prevent oil from reaching the beach and inter-tidal zone is their use in the Christos Bitos incident (7).

The variability of sea conditions, as well as the size of a spill are two of the major factors which often inhibit the containment and recovery of spilt oil. If about 2000 barrels (84,000 gallons) of Bunker C oil were spilt on a calm sea on a windless day, and if no action is taken for about three hours, the circumference of the spill would be approximately 6300 feet. Consequently, this size of a spill would make deployment of sufficient oil booms a rather formidable task. Their use, in many cases, has not prevented oil from reaching biologically sensitive areas.

1.2 DISPERSANTS

Dispersants specifically designed for use on oil spills are relatively new and most of these have been developed since the time of the Torrey Canyon in 1969. They are found under various names - dispersants, emulsifiers, detergents and degreasers, however, those specifically designed to combat oil spills are normally referred to as dispersants. Dispersants are compounds which emulsify, disperse or solubilize oil into

the water column or act to further the spreading of oil slicks to facilitate dispersal of oil into the water column. They consist of three primary components: surfactants, solvents and stabilizers. Surfactants decrease the interfacial tension between the oil and water, thus allowing the oil to more easily spread and be dispersed into small globules. Surfactant molecules are composed of hydrophilic (water compatible) and lipophilic (oil compatible) groups. They can be divided as to being either anionic, cationic or non-ionic. The anionic surfactants compose the largest group in use since the anion is quite surface active. Usually these dispersants are alkalai salts of sulphates or sulphonates. Cationic surfactants have a low surface activity as do the non-ionic ones. However, the non-ionic ones have been found to be the most effective for dispersants for salt water oil spills, being composed of fatty alcohol condensates, ethylene oxide being the most common (7).

The second primary component of a dispersant, the solvent, comprises the bulk of the product. The solvents enable the active agent (surfactant) to mix and penetrate into the oil to form an emulsion. The solvents range in base from petroleum to water, petroleum solvents being the most toxic, but the ones which dissipate most rapidly in a water environment.

A certain amount of mechanical mixing energy is generally required to get the dispersant oil mixture into the water column. Early in their use, helicopters, tugboats or other large powerful ships were used in an effort to cause dispersion. In the United Kingdom, the use of batter boards towed behind boats have proved effective. Obviously in high sea conditions, the mixing energy is no problem. Under such high sea conditions, dispersants have been found to be very effective. There are also self-mixing dispersants available. A self-mix dispersant utilizes the diffusion energy of the surfactant, acting at the oil-water interface.

1.3 PROGRAM INTRODUCTION

The results of this program describe an approach to estimate the environmental impact of an untreated oil spill versus a spill treated with dispersant. It is holistic, in that it combines the physical, chemical, microbial and macro-fauna responses to a spill. The results reported herein represent the findings of a four year effort that integrates mathematical, laboratory, meso-scale in-situ experiments and analyses. The in-situ analyses came as a result of responding to three spills of opportunity. These are the Argo Merchant which grounded on the Nantucket Shoals in December 1976, the Bouchard spill that occurred near the entrance of the Cape Cod Canal in ice-choked Buzzard's Bay in late January 1977 and the fire/oil spill that occurred at the Strategic Petroleum Reserve facility at West Hackberry, Louisiana on September 21, 1978. The investigation of this latter incident was supported under separate contract with the Department of Energy and a final report is being issued (8).

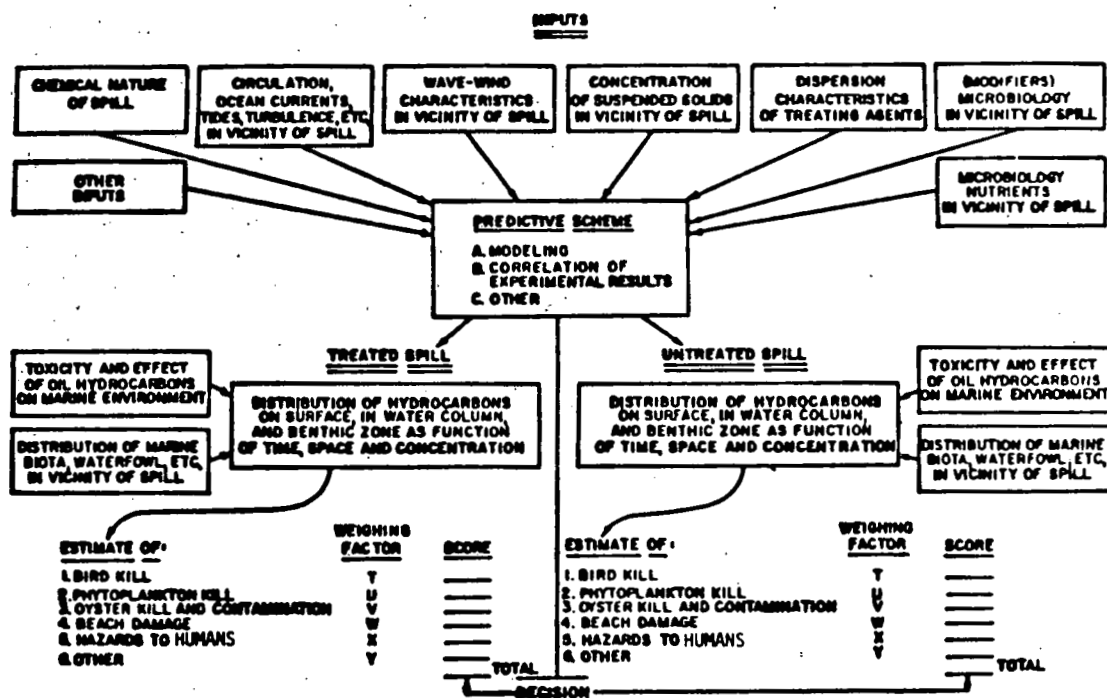
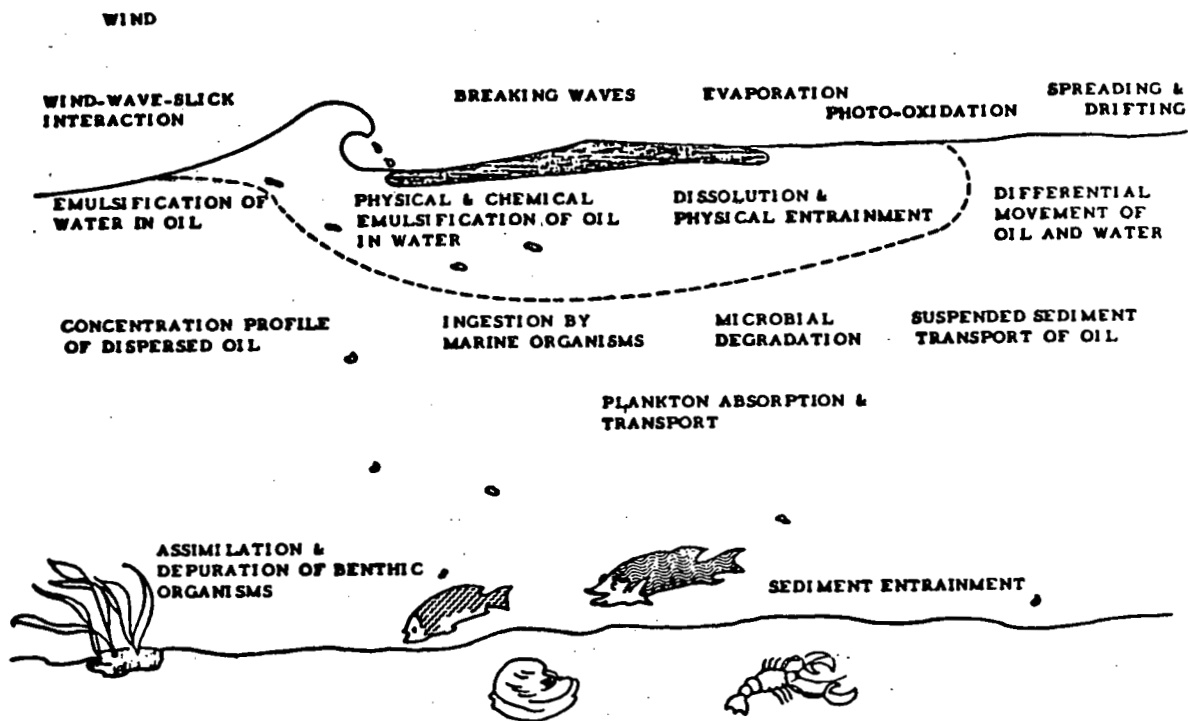
Many models and investigations have been conducted in the past concerning the environmental impact of spills, but none presently available encompasses the breadth and depth required to make a decision as to whether or not dispersants should be used. This program has been designed to provide some guidance in this direction. In spite of this,

there are still many unanswered questions concerning the impact of an oil spill on the environment. The fate and effects of an oil spill, whether treated with dispersants or not, depends on many complicated factors. First, the chemical composition of any oil is extremely complicated and they are composed of many different aromatic, aliphatic and alicyclic compounds (9). Even among the crude oils, the physical properties and chemical composition can vary greatly, and consequently, any refining of these crudes produces even more diverse properties. Since there is such diversity, it is difficult if not impossible to make anything but general statements concerning the effects of oils on specific marine biota. Secondly, because of our lack of understanding of the environment, specifically cause and effect relationships, predator-prey relationships, etc., one can only make some isolated estimates of impacts on specific species. Even this is difficult because the organisms in a real spill are exposed to time-varying concentrations and varying chemical composition caused by natural weathering of the oil which includes evaporation, dissolution, etc., while available toxicity data seldom include these effects.

The approach in this program has been to attempt to mimic the natural weathering and entrainment processes and to expose the organisms to varying concentrations from lethal to minimal sublethal dosages and to study predator-prey relationships under these conditions.

1.4 PROGRAM DESCRIPTION

As mentioned in the above paragraphs, the problem of assessing the impact of an oil spill on the marine environment is a formidable task at best, especially if the objective is to assess both short and long range impacts. Damage assessment such as clean-up costs, losses to business, etc., are much easier to assess after the fact and certainly much more tangible than those associated with losses in fish catch, etc. In the latter type of assessment, a holistic and implicit approach is mandatory. This type of approach requires a determination of the temporal and spatial history of the spill, coupled with the physical, chemical and biological processes that affect the nature of the spill as shown in Figure 1.1. Some of the input that must be considered in this type approach is shown in Figure 1.2 which is a simple version of the decision making process to treat or not to treat a spill. The most important aspect of this procedure is the realization of the strong interdependency of all of the processes. Microbial utilization is both a function of the chemistry and spatial distribution of the oil and other nutrients, whereas the spatial and temporal distribution is a function of wind wave activity, currents etc., and the physical and chemical properties of the oil. The impact of a spill on marine organisms is also a function of the chemical, temporal and spatial distribution of the oil. The traditional bioassay work based on LC₅₀ on 48, 72 or 96 hour tests are of limited value because the tests are static and seldom are these organisms exposed to constant concentrations in the real environment with the exception of some spills in marshes and beaches. Some knowledge of the lethal concentrations as a function of time, together with the temporal and spatial distributions of both the oil and organisms, permits a first order assessment of the number of organisms destroyed as a direct result of the spill. Of secondary importance is the cumulative effect of varying concentrations on the organisms with time as well as sub-acute effects on



behavior and reproduction.

The program was divided into three major but integrated groups, one to study entrainment and evaporation processes, a biological group including microbiology to study the effects of treated oil versus untreated oil on selected marine organisms and oil degradation rates and a third group to provide the chemical analysis. Laboratory type tests were conducted by each group to study some of the fundamental processes, however, all groups participated in the combined tests conducted in the meso-scale facilities as described in the next section. Spills of opportunity provided experimental data to correlate with meso-tank results.

1.4.1 MESO-SCALE TEST FACILITIES

The meso-scale test facility is composed of three twenty-foot high by three feet in diameter fiber glass tanks as shown in Figure 1.3. A schematic of the tank is shown in Figure 1.4. The facility is located adjacent to Narragansett Bay. Salt water is pumped either into the top or bottom in batch operations or in a continuous flow mode. The tanks are wrapped with a coil for fresh water closed cycle cooling and insulated by three inches of polyurethane foam. This type of cooling was chosen because it was capable of providing a uniform temperature distribution of the tank, void of any cold or hot spots. The heat sink for the closed cycle cooling system is a coil submerged in Narragansett Bay. This system is capable of maintaining the water in the tanks to within 1°F of the Bay temperature. Thus, temperature stresses on marine organisms in the tank were minimized. The cooling coils were made in three sections to allow them to be operated in a series or parallel mode. Using this approach, virtually any temperature distribution could be achieved from a stratified layer to a uniform distribution.

Mixing in the tank was provided by submerged oscillating annular disks as shown in Figure 1.4. The amplitude as well as the frequency is adjustable, making it possible to obtain a wide variety of mixing conditions in the tank. Generally it was adjusted so as to provide mixing in only the upper ten feet of the tank. This roughly corresponds to the subsurface circulation caused by an ocean wave having a wavelength of thirty feet.

Bottom dwellers such as scallops were lowered in a basket to prescribed depths before the surface was oiled. To prevent contamination of the scallops when retrieving the basket, a cylindrical section of teflon approximately a foot in height was installed at the water/oil - air interface. When samples were to be retrieved, the teflon section was collapsed across the surface thereby sweeping the oil to one side of the tank, leaving a clean surface through which the samples could be collected.

Water column samples were collected from taps located every twenty-four inches along the length of the tank.

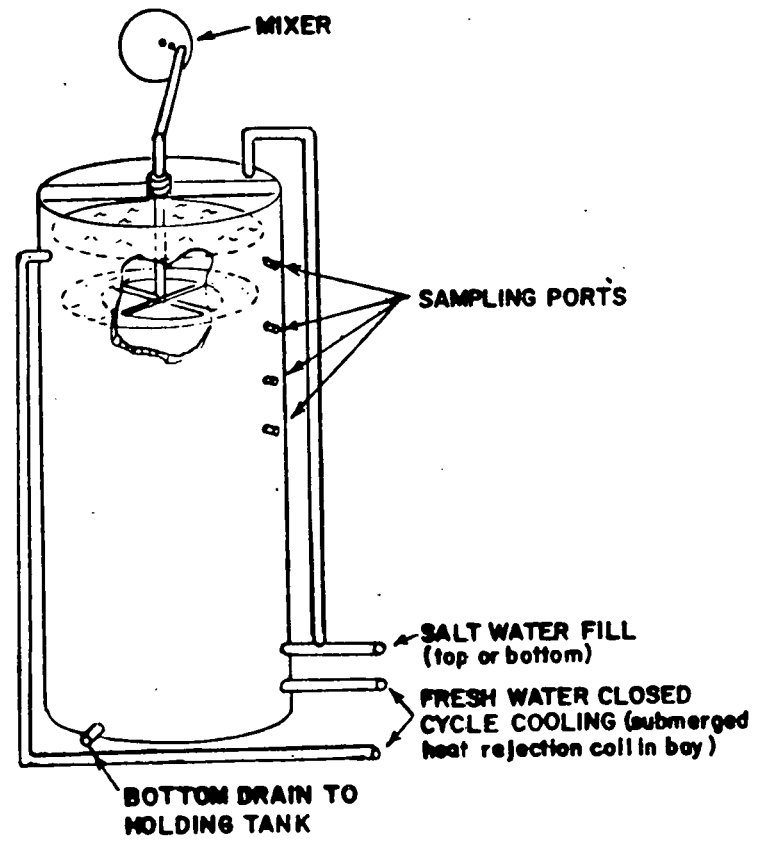
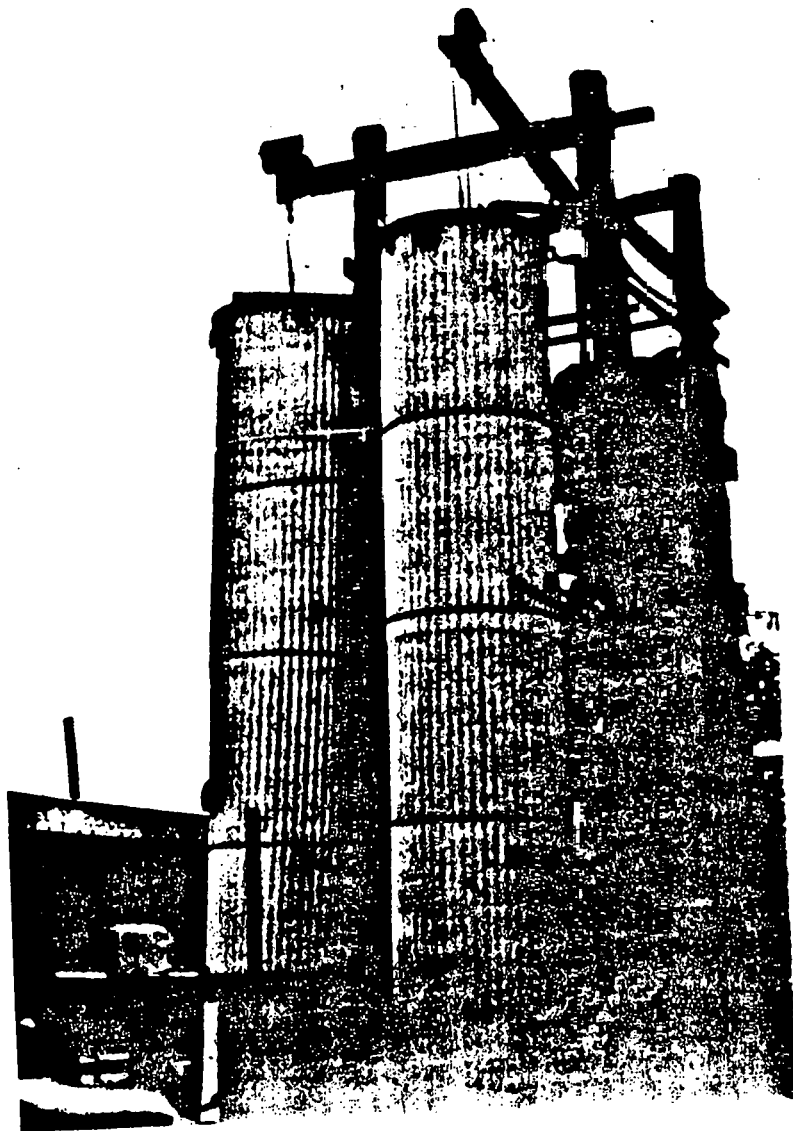


FIGURE 1.4: MESO-SCALE TANKS

1.4.2 ENTRAINMENT, DISSOLUTION AND EVAPORATION STUDIES

One of the primary goals of the program was to determine the temporal and spatial distribution of the treated and untreated oil, hence a comparison of the toxicity and impact under both sets of conditions. Much work has been done in the drifting and spreading of the oil but only limited amount of predictive information is available for entrainment of the oil into the water column and sediment.

In an attempt to gain a better understanding of the combined evaporation, dissolution and overall entrainment process, a series of experiments was designed. These ranged from basic measurements of interfacial tension to combined wind/wave experiments. These experiments and their role in the overall program are described as follows and the section of the report in which they are covered is identified.

INTERFACIAL TENSION

Since entrainment is primarily caused by work done against interfacial tension, a knowledge of the effect that the dispersant has in this property is fundamental to any of the entrainment processes. A series of different types of approaches to measure this property was considered.

The capillary-height method is probably the simplest method available. When a capillary is inserted below the interface of a two liquid system, due to the excess free energy of the interface, the liquid in the lower layer rises to a higher level within the capillary. But for the crude oil water system under study, this method could not be used as the darker upper layer of the crude prevents observations of the capillary height.

In the drop weight method, drops are allowed to form at the top of a capillary immersed in another liquid. From a knowledge of the dimensions of the drop and its weight, it is possible to calculate the interfacial tension. Since drops have to be formed at a finite site, this method is not applicable in systems where a surfactant is present.

The ring method consists of a platinum ring which is pulled up from the interface of the liquids whose interfacial tension is to be measured. The force that is necessary is measured by a torsion balance. Because of problems encountered in obtaining repeatable results in using this method as well as the reasons stated above in the drop weight method, it was decided to investigate other methods.

The bubble pressure method measures the pressure difference across a bubble or drop in another liquid which is proportional to the interfacial tension. Since this is a dynamic method and is difficult to obtain accurate results, it was decided to use the following method.

The pendant drop method is the one chosen to measure the interfacial tension. It consists of making a drop form at the tip of a capillary tube and "letting" it hang in the second fluid. If the density difference is not appropriate, the drop can be made to rise up from the tip of the capillary rather than let it hang. The shape of the drop reflects a balance between interfacial tension and the gravitational forces and can

be used to measure the interfacial tension. The static nature of the method makes it suitable for use where diffusional effects are involved. This method and the results are fully described in Section 12.1.2 of this report.

DROP SIZE DISTRIBUTION, COALESCENCE AND STABILITY OF THE OIL-IN-WATER EMULSION.

Of primary concern is the effect that dispersants have on the formation of stable oil-in-water emulsions and the drop size distribution. The drop size distribution, although not a direct measure of stability, is indicative of the type of emulsion formed and can be used in interpreting the results of other experiments. To measure the mixing energy and drop size distribution, a standard impeller technique was chosen. Total concentration of hydrocarbons in the water column was taken by extracting the water samples with carbon tetrachloride and measured by infra-red spectroscopy. The drop size distribution was measured photographically. Stability and coalescence was determined by measuring the concentration of oil in the water column as a function of time following formation of the emulsion. The complete description of this process and the results are given in Section 2 of this report. Stability of the emulsion was also investigated in Sections 3 and 4 of this report by measuring its settling or creaming rate.

ENTRAINMENT PROCESSES: THE WIND/WAVE EXPERIMENT, THE RAINDROP EXPERIMENT, EVAPORATION AND STABILITY

The real world entrainment process of oil and treated-oil slicks is extremely complicated, and is probably one of the most least understood of the processes that have a major effect on the fate of an oil spill. The complex wind/wave interaction, wave dynamics and currents in the ocean will effect the rate of entrainment and stability of the oil-in-water-emulsion. The addition of a dispersant enhances entrainment processes, but also relies either on mechanical or chemical forces or a combination of both to incorporate the oil into the water column. Furthermore, addition of a dispersant increases the oil slicks spreading properties, thus making the slick thinner and more easily dispersed. For the most part, this project has been concerned with oil and water emulsions and has not concentrated efforts on the formation of water-in-oil emulsions such as "chocolate mousse."

The stability of the oil-in-water suspension (or emulsion) depends on many factors such as the degree of subsurface mixing, the concentration of the oil, the size distribution of the oil droplets, the concentration of plankton, the concentration and type of suspended sediments, etc. Mousse, on the other hand, is a water-in-oil suspension (emulsion) and is generally thought to be much more stable than oil-in-water suspensions. To understand the differences as well as the similarities of these processes, they are discussed in some detail in the following paragraphs.

The important factor that links oil-in-water and water-in-oil emulsions is the type of emulsifying agent that may be found in sea water and naturally occurring in the crude oil, as compared to manufactured oil emulsifiers. The physics of formation of oil-in-water emulsion is the same as the formation of water-in-oil emulsions. Whether one or the

other is formed depends on the type of emulsifying agent present during the process. It is well known that soaps of univalent metals give rise to oil-in-water emulsions, while multivalent metals favor water-in-oil emulsions (10). Whether or not this is the case with respect to crude oil in sea water is yet to be proven. However, Kuwait crude which is well known to easily form "chocolate mousse" also has a higher concentration of organic-multivalent hydrocarbons than most other crudes. As previously stated, the water-in-oil emulsion was not studied in this program, however it was observed in some of the experiments, especially the wind/wave experiment reported in Section 3 of this report.

Suspended sediments can play a role in the emulsification process. It can be easily explained in the following manner (11,12) and involves the interfacial tension between the solid and water, the water and oil, and between the solid and oil. If the surface tension between the solid and oil is greater than the sum of the surface tensions between the water and oil and solid and water, the solid will remain suspended in the aqueous phase. If the surface tension between the solid and water is greater than the sum of the surface tension between the water and oil and solid and oil, the solid will remain in the oil. If the surface tension between the oil and water is greater than the sum of the surface tension of the solid and water and solid and oil, the solid will concentrate on the boundary.

It is known that clay sediments tend to incorporate oil into the water column. Conversely, fine grain sand is generally found in tar balls.

Physical entrainment and stability of the oil-in-water suspension was studied both from an experimental as well as an analytical viewpoint and is discussed in some detail in Section 4 of this report. The "entrainable" particles depend, for most of the systems studied, on particle size distribution and subsurface circulation. Except for the case when there exists a chemical stabilizing agent in the dispersant, the oil droplets, generally having a density less than water, and tend to rise to the surface. Hence, most oil-in-water suspensions are basically unstable and require some degree of agitation or circulation to maintain them in suspension. In the natural environment, quite often the circulation beneath waves, etc., is sufficient to maintain the fine droplets in suspension as with the case in most of the experiments conducted in this report. Subsurface circulation was studied analytically and the results of this study are presented in Section 4 of this report.

The wind/wave experiment was designed to study the effects of waves, and wind blown waves on the entrainment of oil droplets. One of the conditions for the experiment was to allow the action of waves and wind to occur over a sufficient period of time to allow the natural weathering of oil to take place. Initially, it was conceived to produce waves and an air flow in an annular type of wind tunnel. A small scale experiment was designed and conducted. The major problem encountered during the initial test was that oil collected on the inner wall due to circulation in the tank and wind activity. It was, therefore, decided to use a cylindrical tank as described in Section 3. of this report. The particular arrangement chosen allowed the surface slick to undergo wind/wave action for

indefinite periods of time without contacting the walls of the container. It consisted of a tank eight feet in diameter and approximately four feet in height, having the same capacity as the meso-scale tanks previously mentioned. A doughnut shaped wave maker oscillating vertically produced the radially inward moving surface waves. Its frequency and amplitude could be varied so that different wave heights and wave lengths could be achieved. Air flow was provided by an exhaust hood placed over the tank. Subsurface water samples could be collected in similar fashion as in the meso-scale tanks. Radial traverses of oil concentration were also conducted utilizing glass rods inserted through the sampling ports. The results of these tests and a complete description of the experiment are given in Section 3 of this report.

Another entrainment process investigated was the study of entrainment caused by the penetration of an oil slick by water droplets. These droplets can be formed by breaking waves or be due to rain. A description and the results of this experiment are given in Section 4 of this report.

Evaporation from oil slicks is part of the natural weathering process. It is also a fractionation process since the lighter, more volatile components evaporate most readily. Evaporation rates as well as definition of the components are reported in two sections of this report, Section 7 and Section 12.4

1.4.3 OIL SPILL TREATMENT STRATEGY

This particular portion of the project was to use an oil spill fates model as a tool to analyze the effect of various treatment strategies on the fate of a simulated spill. The location of the spill was chosen at the center of the Cod spawning region of Georges Bank and at a time, mid-winter, to affect a maximum impact on the Cod fishery. The output of the model resulting from these simulations was used as input to a fisheries model and is discussed in detail in Section 6 of this report. The oil spill fates model and treatment strategy is presented in Section 5 of this report. The fates model was basically used as a method to show the difference between the spreading characteristics of a surface spill and the diffusional subsurface current driven treated spill, as well as to estimate the concentration distribution of each. The fate model includes most naturally occurring processes as well as the effects of clean-up, removal and dispersion actions and could be used in "real" time to aid the On-Scene-Commander (OSC) in control and clean-up of a spill.

1.4.4 FISHERY-OIL SPILL INTERACTION MODEL

An oil spill-fisheries impact model was developed to obtain an order of magnitude estimate of the impact of a treated versus untreated oil spill. To what extent oil spills at sea affect the commercial catch over the ensuing years and under what circumstances, if any, treatment with a dispersant will mitigate the effect, are addressed in this research. The model estimates first order, direct effects of an oil spill on a commercially fished population. The primary effect is assumed to occur through egg and larval mortality. The biological impacts model formulated contains as subcomponents a population model of the fishery, a model for advection and diffusion of oil and fish larvae which is coupled to the oil spill behavior and fates model described in the previous section.

The model was used to simulate nine variations of an oil spill scenario on Georges Bank, producing a rough sensitivity analysis of system response. Following an overview of the model system, the results and implications of these simulations are discussed along with limitations of the approach used. It is suggested that the most significant unknowns in the system are the parameters governing recruitment dynamics in the fishery, toxicity threshold values and oil entrainment rates being of secondary importance in open ocean conditions.

1.4.5 CHEMICAL ANALYSIS

The overall objective of the project was to address the environmental impact of chemically treated vs. untreated oil spills. The primary objective of the chemistry group was to determine the amount and compositions of petroleum chemicals in the atmosphere, surface waters, water column and sediments resulting from a treated and untreated spill. To meet with this objective it was necessary to develop sample collecting, extraction and chemical analysis methods. In addition, extensive development and testing computer software was required to collect and massage the analytical data. Laboratory experiments were designed and executed to aid in the development of these analytical techniques. Results from the laboratory studies determined the techniques which would be applied to the analysis of the meso-scale experiment and eventually to any "real world" spills of opportunity. The major portion of the chemical analysis is reported in Section 2 of this report. Other chemical analysis techniques developed for quantitatively distinguishing the dispersant from Kuwait Crude by both infra-red and gas chromatography techniques are reported in Section 8 and 12.2.

1.4.6. MICROBIAL DEGRADATION

The study of microbial degradation of hydrocarbons was deemed an important area of investigation. Since the use of dispersants greatly increases the surface area of the oil, making it more susceptible to biological degradation and hence, an important question to answer if dispersants are to be used. The hydrocarbon degradation potential of ocean environments has not been adequately defined, however, it is known to be influenced by such factors as the number and types of hydrocarbon degrading microorganisms, the degree of oil dispersion, temperature and nutrient availability. Hydrocarbon degradation rates measured in the laboratory have been misleading since they were found to be considerably higher than in situ rates. Consequently, microbial utilization of the hydrocarbons was measured in the meso-scale tanks which most closely approach the real environment. A series of other tests was conducted in the laboratory to gain a better understanding of the process. The details of the experiments and results are reported in Section 8 of this report.

1.4.7 BIOLOGICAL INVESTIGATIONS

This portion of the investigation was to study the effects of realistic concentrations of oil and oil-dispersant mixtures on marine life. The impact of a spill on marine organisms is a function of the chemical, temporal and spatial distribution of the oil. The traditional bioassay work, based on LC₅₀ on 48, 72 or 96 hour tests are of limited value in estimating the impact of a spill, because they are static and seldom are

these organisms exposed to a constant concentration in the real environment, with the exception of some spills in marshes and beaches. Furthermore, most of these tests are conducted with unweathered oil, thereby exposing these organisms to the more volatile and toxic components. The approach in this study was to determine lethal concentrations as a function of exposure time. Knowing the temporal and spatial distribution of both the oil and organisms allows a first order assessment of the number of organisms destroyed as a direct impact of the untreated or treated oil spill. It was also recognized that other important parameters that could affect the impact of a spill depended on predator-prey relationships that could cause mortality even when the organism survives the spill. The experiments and results are given in Section 9 of this report.

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2.0 Effect of Chemical Dispersants on the
Stability of Oil Water Emulsions

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Section 12.1.2 Appendix B

1. Measurement of Interfacial Tension
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6. Concentration of Corexit in Water by Volume

Nomenclature

A -	Interfacial Area
d -	diameter of the drop
D -	diameter of the impeller
Fr -	Froude Number
g_e -	acceleration due to gravity
g -	gravitational constant
N -	number of the revolutions of the impeller per minute
n -	number of drops of diameter d
O -	Order of magnitude
P -	rate of power input
Po -	Power number
Re -	Reynolds Number
v -	velocity of the drop
α and β	phases α and β
ϵ	error in measurement of any quantity
ϕ	hold-up
μ	Viscosity
σ	Interfacial Tension

Subscripts

AM -	arithmetic mean
SM -	Sauter Mean
i -	component i

2.1 Introduction

In recent years oil spills on the high seas and inland waterways have been given increased attention because of their adverse ecological and environmental effects. It is estimated that over sixty percent of crude oil consumed all over the world is transported over water. In view of this enormous volume of oil conveyed over the seas and inland waterways, chances of oil spills are great indeed.

Retention and cleanup of oil has met with limited success so far. Mechanical methods are cumbersome and transportation of the equipment is difficult, slow and expensive. On the other hand dispersants and surface-active agents are easier to transport and use, and have met with success in Europe. There has been considerable controversy regarding the use of dispersants to break up oil spills. It has been known that chemical dispersing agents, which are surface active agents, often do more damage than the oil which they tend to disperse (44).

The effectiveness and practicality of chemical dispersants have been seriously questioned since their initial use. In support of this, two well-known incidents are cited often - the Torrey Canyon and the Santa Barbara spills. In both cases substantial quantities of dispersants were used. In both instances there was extensive contamination of the environment.

Unlike mechanical methods which seek to isolate and remove oil from the water surface, dispersants break up the oil into tiny droplets. Oil in this condition is considered to be amenable to biodegradation (18).

Biodegradation of oil is a rate process and depends upon interfacial area and time. For biodegradation it is desirable that we have the smallest droplets possible and have them stay in the water column for the longest duration of time. It is here that the stability of the dispersion becomes important. Stability of the dispersion can be defined as a fraction of the hold-up or interfacial area. (Hold-up can be defined as the fraction of the dispersed phase in the continuous phase.) Since interfacial area is a function of hold-up, interfacial area alone can be thought to be a criteria for stability of the emulsion.

It is the intention of this investigation to evaluate the effectiveness of dispersants in distributing and stabilizing crude oil in the water column.

2.2 Literature Survey

Previous work on the dispersants to break up oil into small droplets is of relatively recent origin. In a recent investigation Jasper, Kim and Wilson (42) studied the effect of dispersants in breaking up a crude oil into fine droplets. They used two dispersants, a self-mixing type and a conventional one. The conventional dispersant is a surface active agent which merely reduces the interfacial tension. The new generation

'self-mix' dispersant on the other hand is expected to produce spontaneous emulsification. This type of surfactant is predominantly soluble in the oil-phase. When the oil comes into contact with water, that part of the surfactant that has a strong affinity for water tends to diffuse to it. During this process it carries droplets of oil into the water phase. The self-mix type and the conventional dispersant were found to perform differently, with the self-mixing type creating a better dispersion. The study revealed that the self-mix type dispersed oil more efficiently as the rate of energy input decreased. Further it was found that a finer dispersion was possible using a self-mix dispersant. The study by Jasper et al also showed that there was minimal increase in hold-up with increase in power input.

In the past, investigations in this area have been conducted with an entirely different goal in view. In liquid-liquid extraction operations two immiscible phases are brought into intimate contact, and when equilibrium has been achieved, allowed to separate in a settler. Here, instability of the dispersion and not stability is the consideration. There is yet another striking difference between traditional extraction operations and the situation encountered in an oil spill. In extraction operations the hold-up is of the order of 10 to 50 percent. In the present investigation the hold-up is of the order of parts per million. However, since coalescence and break up of droplets are basic to both situations they will be considered in this survey.

The earliest investigation on the coalescence of droplets concerned the behaviour of a single droplet resting on a plane liquid surface. This is conceivably the simplest possible situation. Reynolds (1) began the study of coalescence by observing the behaviour of a rain drop resting momentarily on the surface of a pond. The findings were rather qualitative in nature. This observation was followed by Smoluchowski (2) who analyzed the rate of coalescence of droplets in dispersions and developed an idealized model for the rate of coalescence of droplets. Apart from the above two studies there had been no significant contributions in this field until the second half of this century.

The latter half of the twentieth century saw a burst of research activity in the field of coalescence. It should be noted that the bulk of research in this area has been confined to coalescence of single drops. This is understandable because all factors involved in the coalescence of single droplets should be identified and their significance estimated before coalescence of swarms of droplets can be studied. Thus all workers found that the time interval of the arrival of a drop at the interface and its disappearance into its parent phase is not constant; but there is a distribution of times - the distribution being approximately Gaussian. Further all researchers agreed that the coalescence process includes five consecutive stages. These are

- (i) the approach of the drop to the interface, resulting in the deformation of both the drop and the bulk phase
- (ii) damped oscillation of the drop at the interface
- (iii) the formation of a film of the continuous phase between the drop and its bulk phase
- (iv) drainage of the film, its rupture and removal with the initiation of the coalescence process proper and

(v) transfer of the contents of the drops partially or wholly into its bulk phase. Most workers assumed (without much evidence) that stages (i) and (ii) took place immeasurably fast so that the time of coalescence was the time taken for stages (iii), (iv), and (v) during which the drop rested on the thinning film at the interface. Some workers called this the rest time.

As has been stated above, for drops of the same size and physical properties coalescing under identical conditions there is a spread of coalescence times. This suggests that a large number of experiments had to be carried out in order to get the distribution. Gillispie and Rideal (3) found that about 100-200 drops had to be observed to get reproducible results whereas Jeffreys and Hawksley (4) using more refined apparatus found that it was necessary to study only 70-100 drops to get reproducible results. Working with drops stabilized with surfactants, Cockbain and McRoberts (5) were able to obtain reproducible distribution curves using only 30 drops. In the study of coalescence time, researchers have defined two means, namely the arithmetic mean of the time of coalescence (of identical drops of course) and half rest time which is the time taken for half the drops to coalesce. Generally half rest time has been found to be more reproducible than the arithmetic mean and the ratio of the arithmetic mean to the half rest time has been found to be greater than one (in the range of 1.01 to 1.27.)

A drop residing at the interface may coalesce completely or it may coalesce partially, producing a smaller drop which will ultimately behave in a manner similar to the parent drop. That is, it will coalesce producing a smaller drop and the process may continue for as many as six or seven times. This phenomenon is known as stepwise coalescence. It was first observed by Wark and Cox (6) during froth floatation experiments and a little later by Mahagar (7) during experiments at the air-liquid interface.

The coalescence of a single droplet at a plane interface is accomplished through the drainage and rupture of the film of the continuous phase. Therefore the factors that most affect drainage and rupture, control the coalescence process. These factors have been tabulated by Lawson (8).

Nearly all workers studying coalescence agree that coalescence time increases with drop size. A larger drop tends to flatten into an oblate spheroid when resting on the interface so that the film between the drop and the interface is increased in size and thereby the drainage time is increased also. Moreover, interfacial area between a larger drop and the interface is larger for the large drop so that the resistance to drainage is larger and the coalescence time is greater. It should be pointed out that Lang (9) found by theoretical analysis that the thickness of the film at the instant of rupture is independent of drop size. Neilsen, Wall and Adams (10) found that for some three component systems the stability of the drop increased with increased size. This would clearly depend on the nature of the third component. A diffusing solute would increase or decrease the stability of the drop depending on the direction of mass transfer.

A number of investigators have found that the settling distance through which the drop traverses affects the coalescence time. Nielsen (10) reported that the coalescence time was independent of the distance through which the drop traverses, while Lang (9) suggested that the distance of fall (or rise) could either increase or decrease the stability of the drop depending on the mechanical disturbances produced. However Lawson (8), Hawksley (11), and Jeffreys and Hawksley (4) have shown that the stability of the drop increases with increase in the distance of fall. It is widely accepted that the coalescence time is proportional to the distance that a drop traverses raised to an exponent n . The exponent n increases with drop size but is independent of temperature. It is only the first step of coalescence that is affected by the distance that the drop traverses although many workers have reported that the distance of fall also affects the other steps to a large extent. There are several explanations to the above mentioned observations:

(i) The drop may acquire an electrostatic charge during passage through the continuous phase. The extent of this charge increases with the distance of descent, thereby offering a greater resistance to the drainage of the film. This seems to be a perfectly logical explanation. However, McDonald (12) found no pronounced effect of electrostatic charge except on very large drops.

(ii) Drops passing through the continuous phase collect small quantities of surfactants which tend to increase the stability of the drops. The greater the distance travelled, the greater the amount of surfactant collected. It should be pointed out that if this were the case, reproducible results would never have been possible by using different batches of the same chemical. As different batches, however carefully controlled in production, contain minute quantities of surfactants in varying degrees.

(iii) The variation could also be produced by the drop "bouncing" after striking the interface, with the result that rippling of the interface prevents the film between the drop and the interface from draining. However, Hawksley (11) showed that the terminal velocity of most of the drops is attained within fifteen to twenty drop diameters. Since the mean coalescence time continues to increase when the critical distance has been exceeded, this could not be a good explanation.

Curvature of the interface between the drop and the coalesced phase was found to have an effect on the stability of the drops. Nielsen (10) has shown that the stability of the drop increased when the curvature of the coalesced drop phase was concave to the drop. This could be expected because drainage of the film is thereby promoted.

Density difference between the two phases is another factor that seems to have some bearing upon the coalescence rate. Large density differences result in severe deformation of the drop. The drop tends to flatten so that the area of drainage of the film is increased, whereas the hydrostatic force causing drainage does not increase proportionately. These two opposing tendencies tend to cancel each other. In fact, many workers have claimed that the rest time increases with increase in the density difference between the phases.

Phase viscosity ratio is another parameter which influences the coalescence time. An increase in the phase viscosity would be expected to increase the coalescence time as it takes more time to drain a more viscous film. There is experimental evidence to confirm this.

A high interfacial tension results in the drop resisting deformation so that the area for the film to drain would tend to decrease with increase in interfacial tension. Thus coalescence time tends to decrease with increase in interfacial tension. However, an increase in interfacial tension also tends to inhibit the flow of the film itself so that here again there are two opposing tendencies. Generally, coalescence time tends to decrease with an increase in interfacial tension.

Temperature affects all the physical properties that affect coalescence. Generally an increase in temperature tends to reduce coalescence time unless there is a change brought about in the coalescence process. Thus, Jeffreys and Hawksley (4) found that single step coalescence changed to multi-step coalescences in some instances when temperature was raised.

There are conflicting reports on the effect of vibrations on coalescence times. Gillespie and Rideal (3) suggested that vibrations tend to stabilize the drainage film, thereby impeding coalescence. On the other hand Lang (9) proposed that vibrations introduced random variations in the coalescence reported by different workers. Lang and others investigated the effects of extraneous vibrations and found these to be negligible. Brown and Hanson (13) studied single drop coalescence in alternating current fields of different frequencies and they concluded that in the systems they investigated, coalescence time was virtually independent of frequency.

Extensive research has been done on the effect of an external electric field on the rate of coalescence. Charles and Mason (14) applied a direct current field to the drop in such a manner that the force promoting coalescence was several hundred times that of gravity. They found that the drop flattened so that the area of draining the film was greatly increased, but since the force was so large the rate of coalescence was accelerated. Furthermore, they found that when stepwise coalescence occurred, the secondary drop was much smaller.

The presence of electrical double layers affect the rate of coalescence in a significant way. It had been widely observed that the rate of coalescence of drops whose phases contain electrolytes is lower than the rate of coalescence of pure drops residing in pure solvent. This is explained in part by the formation of electrical double layers between the draining film and the drop and the coalesced phase and the draining film. These double layers tend to retard the flow of draining film through the force of attraction of the opposite charges at the interface and in the flowing liquid. This effect has been given the name "electroviscous effect" by Elton and Picknett (14). It will be most pronounced when the thickness of the draining film is of the same order of magnitude as that of the electrical double layer, and when the apparent viscosity becomes five times that of the normal viscosity of the liquid in the draining film. Both Cockbain and McRoberts and Gillespie and Rideal (3) suggest that where double layer effect is significant, small drops should

be more stable than large ones. However, the problem is more complex than suggested by this simple statement because, although the force promoting coalescence is small in the case of a smaller drop, so is the area of the drainage film. Consequently, there will be less chance of the double layer becoming significant.

The presence of a third component tends to accelerate or retard the rate of coalescence. Thus solid substances tend to promote coalescence especially if they are wetted by the drop phase because the solid particle tends to form a bridge across the draining film thereby promoting the rupture of the film. This was demonstrated by Charles and Manson (15) who contaminated a benzene-water interface with minute glass beads. They found that coalescence was instantaneous.

There is a tremendous increase in interfacial area in emulsification; and this makes it necessary to take a look at surface activity. For example dispersion of only 1 cubic centimeter of oil into water in the form of fine droplets of a radius of 0.1 micron size creates an interfacial area of 300 square meters - an increase of the order of a million-fold. Under such circumstances the properties of surfaces and especially interfaces become of great importance.

The notion that surfaces and interfaces behave in a manner different from the bulk of the matter had been known for centuries. Partington (19) cites Leonardo da Vinci in this connection. For many years explanation of surface tension depended on the assumption that the free surface behaved like a contractile skin. Although liquids behave as though such a skin exists it is not really necessary to take such a view. It is the short range attractive forces that are known as van der Waal forces that are responsible for the special behaviour of the surfaces and interfaces. Molecules in the bulk of the liquid experience a balanced force in all directions because the attractive forces fall off rapidly with distance. However, at the interface the molecules experience a net inward pull; and this accounts for the contractile skin-like behaviour of the free surface. When a surface film is increased more molecules are brought to the higher energy condition at the surface. Thus, creating new surface is analogous to the phenomena accompanying vaporization. Stefan (20) was the first to suggest that there would be a relation between surface tension and latent heat of vaporization. Partington (19) gives an extensive list of theoretical and empirical equations relating the two properties.

Surface tension of most liquids decrease with increase in temperature. This is a corollary to the molecular theory of surface tension. The increased kinetic energy acquired by the molecules at the higher temperature will overcome the net attractive force on the molecule. Moreover, at conditions approaching the critical, the cohesive forces between the molecules vanish, and therefore the surface tension will vanish also at the critical. Eotvos (21) proposed a semi-empirical equation, which would predict the surface tension of a wide variety of substances from one empirical constant, the molecular weight and the critical temperature. This equation was improved by Ramsay and Shields (22), who in effect modified the empirical constant in the Eotvos equation.

Interfacial tension is a condition identical to surface tension except that instead of the vapor space above the free surface of a liquid there is yet another liquid whose molecules will exert substantial attractive force on the molecules of the other liquid at the interface. Thus the interfacial tension between two liquids will lie between the surface tensions of the liquids at the same temperature. Dupre (23) suggested an equation for calculating interfacial tension from the surface tension values of the separate phases. But there was the limitation that the two liquids had to be immiscible in each other. Since few liquids are completely immiscible in each other, the interfacial tension values so calculated were not accurate. Antonoff (24) suggested an improvement to Dupre's equation taking into consideration the mutual solubility of the liquids. Recently Girifalco and Good (25) have suggested an equation, based on sound thermodynamic principles, which is in fair agreement with experimental data.

When considering emulsions, it is of far greater importance to look at the effect that solutes have on interfacial properties. The fact that small amounts of solute can have a violent effect on interfacial properties has been demonstrated by Hardy (26). A large lens of petroleum jelly was formed on the surface of pure water. A drop of oleic acid was placed on the lens. After a short time considerable agitation was noticed and then the lens appeared to shatter, with almost explosive violence into small fragments, which were propelled to the edges of the container.

That the presence of a small concentration of solute should have such an effect on the surface tension is not surprising; what is surprising is the tremendous variability of the effects observed. The large lowering of the interfacial tension on the addition of certain types of solutes is due to the fact that the solute concentrates at the interface. The molecules which produce this effect are known as amphiphilic molecules. They are oriented at the interface with their lipophilic portion extending into air (or into a non-aqueous phase). That there should be a higher concentration of the solute which causes the decrease in the interfacial tension at the interface has been proven by Gibbs. The assumptions involved in the derivation of the Gibbs equation have been critically reviewed by de Witte (27), and the rigor of the equation has been criticized by Guggenheim (28). Scatchard (29) reviewed the derivation by Gibbs and concurs with him.

In any mixing operation it is often necessary to know the energy input to the system. There are a number of ways to determine this. Energy input can be directly measured by a dynamometer, by measuring the amperage of the electric mixing motor or by making use of a torque meter. These methods can be expensive, inconvenient or inaccurate. However we can design a 'standard' mixing operation for which power correlation curves are available. When a standard impeller is turned in a liquid, a flow pattern is established in terms of the impeller characteristics, type of fluid and the geometry of the mixing vessel. After this circulation pattern has been set-up, the only way the input energy can be changed is by changing the rate of rotation of the impeller. In other words, the speed of the impeller and the environment it is in controls the input energy regardless of the power capacity of the driving mechanism.

White and co-workers (39) were the first to suggest the possibility of correlating the performance of mixing impellers by dimensional analysis. This idea was later extended by Hixon (40), Johnson and Thring (41) and Rushton and Oldshoe (42). The power correlations give Power number as a function of impeller Reynolds number and Froude number. Power number is given by

$$P_o = \frac{P g_c}{\rho N^3 D^5}$$

the impeller Reynolds number by

$$Re = \frac{D^2 N \rho}{\mu}$$

and the Froude number by

$$Fr = \frac{D N^2}{g}$$

Froude number characterizes the gravity forces and in a well baffled tank it is negligible. In this case the Power number becomes a function of the impeller Reynolds number alone.

2.3 Experimental Set-Up and Procedure

Equipment: The experimental set-up consists of a baffled tank with a turbine-type agitator system. A refrigeration system was used for temperatures below ambient. Other accessories included a temperature controller and a temperature recorder.

The experimental tank (fig. 2.1), made of 'Nalgene', a commercial polyethylene, had a height of 0.6 M and diameter of 0.42 M. The tank was filled up to 0.0757 M³ (20 U.S. Gal.) in all experiments. This corresponds to a height of 0.42 M, thereby giving a height to diameter ratio of 1:1 for the undisturbed liquid. Using the tank for the above mentioned capacity of 0.0757 M³, gave a free-board of 0.18 M - more than adequate to prevent any splashing when operating up to speeds of 600 RPM using a 0.09 M (4 in.) turbine. The tank was fitted with four equally spaced taps made of Polyvinyl Chloride. Glass tubes were attached to the insides of the taps extending to one half the radius of the tank.

Since the experiment involved detection of small quantities of hydrocarbon in the water, the tank prior to use was tested to see if any hydrocarbon will leach out from the polyethylene material. The results

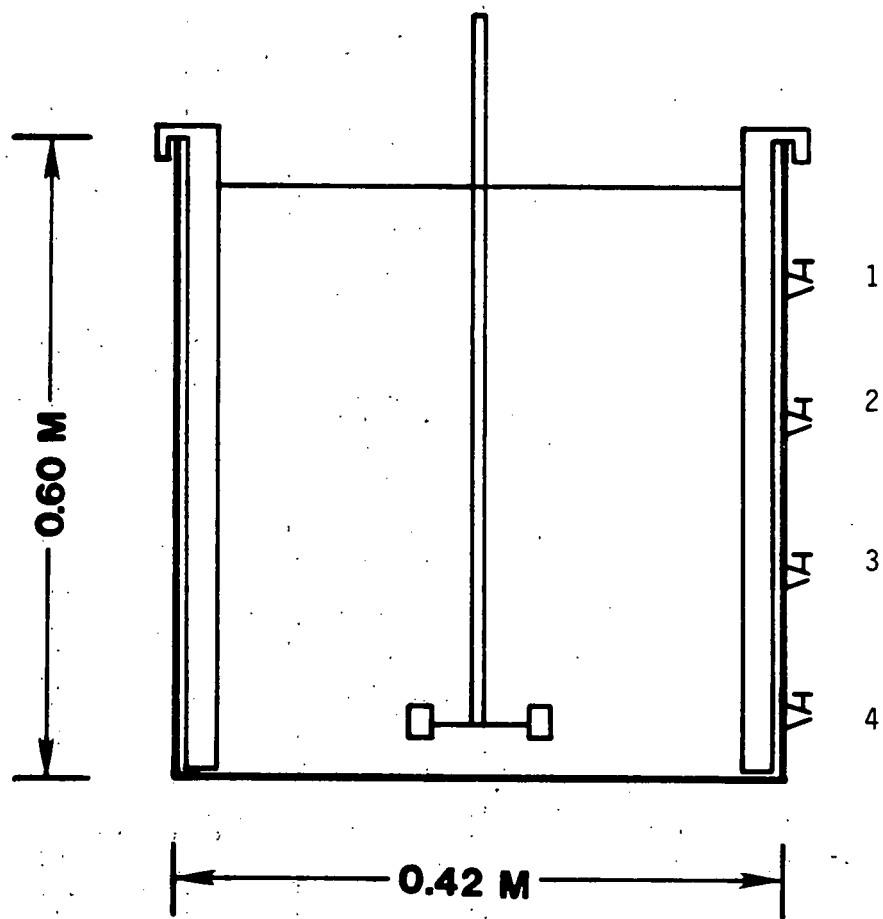


Figure 2.1 Experimental Tank - 20 gallon

were negative.

Four equally spaced rectangular baffles of 1/12 the diameter of the tank, and made of aluminium were used. The baffles were fitted to the tank through a notch and fixed using Allen screws.

The liquid was agitated using a six-blade flat turbine of 0.101 M (4 in) diameter. A d.c. current motor of 0.373 kilowatts (1/2 h.p.) was used to drive the turbine through a shaft of 0.0063 M (1/4 in). The d.c. motor permitted continuous variation of the speed over a wide range. Both the turbine and the shaft were made of stainless steel to protect against corrosion due to sea water.

Samples were collected in 500 ml graduated bottles with glass stoppers. Extractions were done in 0.0005 M (500 ml) separatory funnels, with polyethylene stop-cocks and stoppers.

To study the drops of oil in the water column, photography was used. This method was preferred over automatic electronic counting (using Coulter Counter) because of the necessity of maintaining a quiescent medium for studying the stability of the dispersion. Coulter Counter requires a flowing system. The photographic technique on the other hand requires only small samples from the system. The samples were taken on pre-cleaned glass slides using glass pipettes. Cover glasses were used to prevent evaporation of the samples. A Leitz-Wetzlar microscope (Model No: 512), to which a Nikon camera was attached, was used. The microscope had four objectives: 5, 10, 25, 50 magnification. The ocular had a magnification of 10 thereby giving a maximum magnification of 500 for the microscope. A very slow black and white film (Kodak ASA 32) was preferred, since the static system did not call for a fast film. The slower film gives better drop definition than the high speed film. The size of the drops were estimated by comparison with a scale etched on the objective and photographed along with the drops. The photographs were mounted and projected on a screen for counting.

2.3.1 Extraction of Oil:

The oil in the water column was extracted by carbon tetrachloride. Three aliquots of 10 ml each of carbon tetrachloride was used for each sample. The quantity of oil removed by the carbon tetrachloride was determined by a Perkin Elmer infra-red spectroscope (Model no.: 451). The system was calibrated for the concentration of oil in the carbon tetrachloride. Since the range of the equipment was limited to 40 parts per million of oil, the extract had to be diluted to low concentrations. Spectral grade carbon tetrachloride was used.

A. Materials:

Sea Water: Sea water was preferred over pure water and synthetic sea water, because it was desired to simulate as closely as possible ocean conditions. Pure water devoid of all salts and zoo-plankton commonly found in actual sea water, would have drastically affected surface and

interfacial properties of the dispersion. The synthetic sea water although of consistently accurate composition, differs very much from sea water. The presence of very small quantities of dispersants that are usually found in sea water was not a serious problem as the concentrations of the dispersant used in the experiment was larger by many orders of magnitude. The sea water for the experiments was brought from Narragansett Bay in polyethylene containers and stored in a large "Nalgene" tank.

Crude Oil: A light Kuwait crude was chosen for the experiment. The choice of the crude was governed by the fact that this Kuwait crude had been chosen by many different laboratories for the purpose of studying oil pollution. Also, detailed analysis of the crude had been made by Exxon Research Laboratories and had been made available for the present investigation.

The crude had an API Gravity of 31.4, which would place it in the category of light crudes. Analysis (by Exxon Labs) showed that it had a sulfur content of 2.44 percent by weight and 0.14 percent nitrogen. Nickel and vanadium were 7.7 and 28 parts per million respectively. Analysis by mass spectroscopy showed that the crude was 34 percent by weight saturates and 21.9 by weight aromatics.

A commercial dispersant known as Corexit 9527 manufactured by Exxon for dispersing oil was used. Being a commercial dispersant, detailed specifications of its composition were not available.

Procedure: Sea water from Narragansett Bay was allowed to settle in the tank for a least a day before it was used for the experiments. This allowed any suspended particles to settle out. Ten ml of Kuwait crude was added to the sea water in the tank. In experiments in which dispersant was used, 2 ml of the dispersant was added to the system.

The duration of the agitation was decided from considerations of power input. To have a common basis for comparison, equal power was used in all the experiments, except in the case where there was to be no agitation.

For the calculation of power requirements, recourse was made to the power correlations for six-bladed flat turbines. In the present investigation, we had a two phase system. But power correlations for two phase systems are very sparse. However, Laity and Treybal (31) have suggested the use of weighted property values. Since in the present case the hold-up of the dispersed phase is extremely small, the properties were essentially that of the continuous phase. The power correlations give power number as a function of the impeller Reynolds number. Power number is defined as

$$\frac{P}{\rho N^3 D^5} g_c$$

and the impeller Reynolds number as

$$Re = \frac{D^2 N \rho}{\mu}$$

The power required to turn an impeller at a given speed is a function of not only the fluid properties but also the geometry of the impeller and the vessel. For calculation of power for the six-bladed flat turbine reference was made to Fig. 10.10, 'Liquid Extraction' by R.E. Treybal (32).

Samples were taken in 500 ml graduated glass bottles as soon as the motor was stopped; for the purposes of studying stability a timer was started at the same instant. Four sets of samples were taken, one from each tap, at 0 hrs, 1 hr, 2 hrs, and 24 hrs, and placed in graduated bottles.

Simultaneously, three drops were taken from each tap and placed on pre-cleaned slides and covered. These samples were photographed, 9 shots for each tap at each time.

The samples in the graduated bottles were extracted using carbon tetrachloride. First the 200 ml sample was transferred to a 500 ml separatory funnel. Then the first aliquot of 10 ml carbon tetrachloride was poured into the separatory funnel. To maintain consistency for each extraction the separatory funnel was shaken 20 times by hand. The extract was collected in pre-cleaned dram bottles and labelled. The procedure was repeated with a second and third 10 ml aliquot of carbon tetrachloride.

Since the concentrations usually encountered in the above extractions were beyond the range of the Infrared Spectrometer, 1 ml of the extract was taken and then diluted with 30 ml of carbon tetrachloride.

The photographs were developed and mounted. They were then projected on a screen and the size of the drops estimated by comparison with the scale which was photographed along with the drops.

Interfacial tension between the oil phase and aqueous phase was measured by the pendant drop method. Dynamic methods like the ring method are unsatisfactory because of the presence of surface active agents. When a new surface is formed in a medium in which a surface active agent is present, it will not be in equilibrium as the surface active agent has to diffuse to the newly created surface from the bulk of the medium. This is a consequence of the fact that there is a higher concentration of the surface active agent at the interface than in the bulk of the phase. This makes it necessary to use a method which is static or semi-static.

The pendant drop method consists of forming drops of one liquid in another liquid at the tip of a capillary. The drops are allowed to form at a slow rate so that the new surface will be in equilibrium - or close to being so. These drops were then photographed and their shapes deter-

mined by a shape factor by measuring two of their characteristic dimensions. Interfacial tension is a function of their shape.

Since the oil phase is lighter than the aqueous phase, the drop was allowed to form at the tip of a capillary which was oriented upwards. The capillary was connected to a reservoir which could be moved up or down at will. The capillary was kept in a water bath which was cooled by a refrigeration system.

The shape of the drop was determined by a photographic technique. As the drops formed at the tip of the capillary at the rate of about one drop per minute, its photograph was taken using a Mamiya Sekor camera. The camera had an extension tube attached to its lens to provide a magnification of approximately 10. A scale was photographed along with the drops. This helped in determining the size of the drop and its shape factor by comparison with the scale rather than making use of the magnification of the extension tube-lens system. The photographs were developed and mounted, and projected on a screen, and the size and shape measured.

The differential equation governing the shape of the drop has been solved as a function of the interfacial tension by a number of investigators (33). The numerical solution of the differential equation is available in the form of a table. Reference was made to these tables for the calculation of the interfacial tension (33).

To study the effect of temperature on the oil-water dispersion, a smaller tank was used. A smaller tank was used in preference to the larger 20 gal. tank because the requirements for refrigeration will be within the range of a 0.37 kw (1/2 hp) Haake refrigeration system. The tank of 0.3 M diameter, was made of glass and fitted with four baffles made of aluminum of 1/12 the diameter. Water was filled in the tank up to a depth of 0.3 M, thus giving a depth to diameter ratio of 1:1 for the undisturbed liquid. A free-board of 0.08 M was provided above the free surface of the liquid surface to make allowance for any splashing. The tank was agitated using a six-bladed flat turbine of 0.08 M (3 in) diameter. The impeller was driven by a variable speed motor of 0.06 kw (1/12 hp). The sampling and extraction procedures were identical to that used for the larger tank. The sample was taken from a depth of 0.15 M, using polyethylene tubing and placed into graduated bottles.

2.4. Results and Discussion

2.4.1 Drop-Size Distribution

When two liquids are agitated in a tank impeller system, which of the two liquids become the dispersed phase and which becomes the continuous phase depends on a variety of factors. If the two liquids are in comparable ratio, i.e., 45:55 percent by volume, the liquid that wets the impeller will be the continuous phase. However, when the volume fraction (hold-up) of one liquid is much smaller than the other, i.e., less than 25 percent, it is very difficult to disperse the liquid having the larger

volume fraction. From solid geometry we know that when spheres of equal size are packed together under conditions of closest packing, the volume fraction occupied by the spheres is only 74.02 percent. But when we have spheres of varying sizes, it is very obvious that we can pack much more in a given volume. In fact, emulsions of 99 percent dispersed phase have been prepared (32). However, in the present investigation the question as to which would be the dispersed phase and which would be the continuous phase could hardly arise. The crude oil phase was of the order of 1/10000 by volume of the aqueous phase. Thus the most probable dispersion that may be observed is the oil-in-water type. The hold-up was deliberately kept low so that the system would have about the same hold-up that could be expected in an oil-spill situation on the high seas.

In this investigation, low impeller speeds were used. This was done so that the turbulence generated would be as small as possible. Power correlations of Laity and Treybal (32) give power number for the impeller as a function of impeller Reynolds number. Since it was desired to use as small a turbulence as possible, the impeller Reynolds number just beyond the transition from laminar to turbulent was used. For the tank impeller system, this speed worked out to be 58 rpm (32). Thus the lowest speed that was used was 60 rpm.

It has not yet been established how the phase that is dispersed comes to be broken up into tiny droplets. It has been presumed by many workers that the phase that wets the impeller is the continuous phase (32). If this is the case, then the break-up action of the dispersed phase is due to the shearing action by the continuous phase.

A number of investigators have set an upper limit and a lower limit on the size of the droplets that can be observed in an emulsion. The lower limit is about 0.1 microns - a size approaching molecular dimensions. The upper limit is about 30 microns (30). Drops of larger than 30 microns are difficult to observe in an emulsion because they tend to rise fast and tend to coalesce with the parent phase. In this study attention was focused on drops whose sizes varied between 1 micron and 12 microns. There are a number of theoretical and empirical models available for the calculation of the rate of rise of a drop in a quiescent medium. The Stokes model (36) assumes that the drop behaves like a solid sphere while it moves in another medium. This is an approximation as there are circulations within the droplet. A more realistic model like the Ryczynski and Hadamard model (37) takes into consideration the movement of the fluid within the droplet. This model was used to calculate the rate of rise of a drop of Kuwait crude in sea water. This data shows that for droplets of size less than 12 microns the time taken to rise to the top of the tank would be of the order of less than 10 hours (fig. 2.2). Since an emulsion of oil in water has to be stable for a time of the order of days, it was thought unnecessary to observe droplets of size larger than 12 microns.

Jasper, Kim and Wilson (42), in their investigations on drop-size distribution in oil-water systems had found that drops larger than 6-7 microns are difficult to observe in an emulsion. Further they had concluded that the larger drops are insignificant for determining arithmetic means of the drop-size distribution (43). An extremely large drop would have little effect on the arithmetic mean if the small drops outnumber

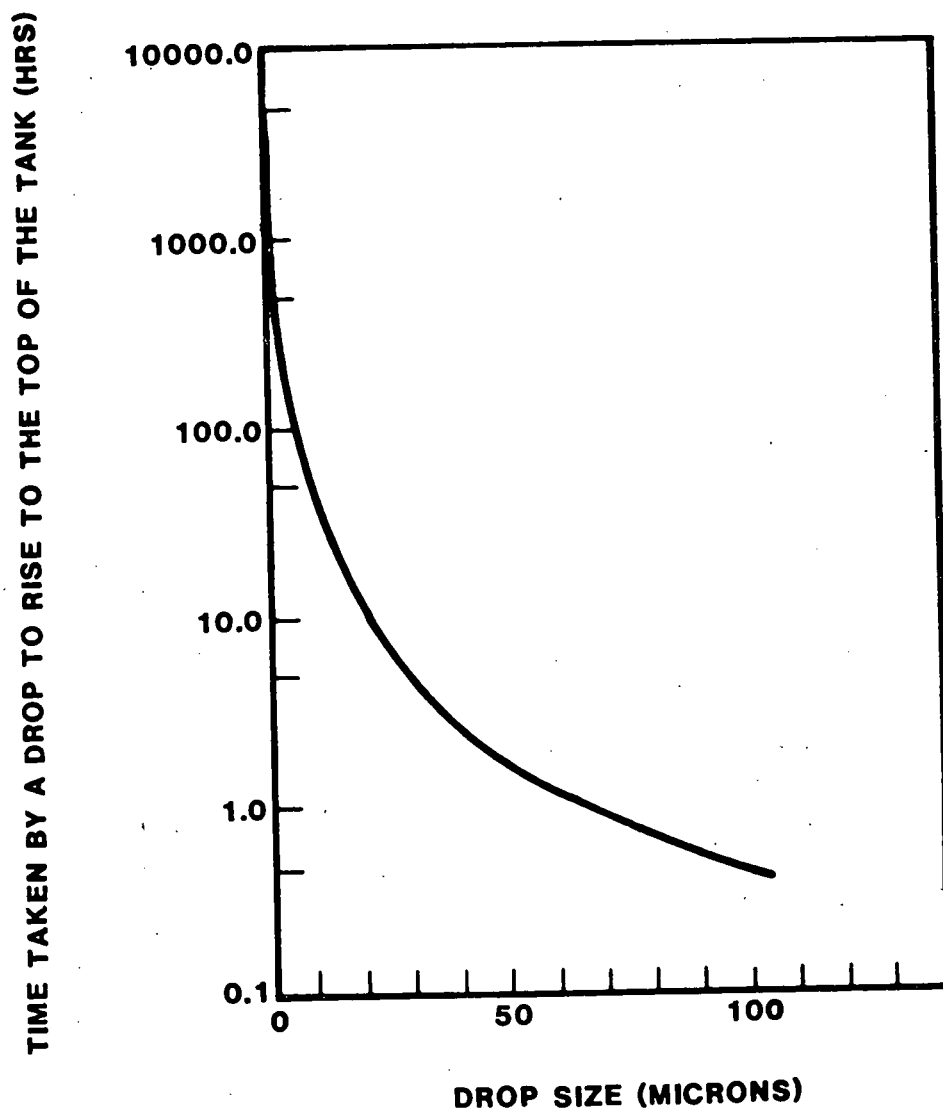


Figure 2.2 Time Taken by a Drop to Rise to the Top of the Tank (hrs).

the larger drops by a large factor. The experimental data (see distribution data in Appendix D) shows that invariably there were much larger number of smaller droplets than there were larger ones.

If the drop size distribution was normal (it is not a normal distribution, but is 'leptokurtic' or left leaning - see the plots of the distribution in Appendix C) then over 95 percent of the drops would be within two standard deviations of the arithmetic mean. For drops of average size, 2-3 microns, this would have meant that over 90 percent of the drops would be less than 7-8 microns. Therefore, taking an upper limit of 12 microns for studying emulsions is considered satisfactory, especially in view of the fact that the distributions usually found in emulsions are left leaning.

The number of drops that are counted for studying the drop-size distribution depends to a large extent upon getting the accuracy to which the distribution is desired. To arrive at a reasonable number, investigations in this area in the past by various workers were relied upon. Gillespie and Rideal (3) had found that it was necessary to observe 100-200 drops to get reproducible results, while Jeffreys and Hawksley (4) and Cockbain and McRoberts (5) using more refined techniques needed only half as many drops. Since all the samples that were counted had more than 100 drops the drop-size distribution is accurate. (See tables 1a thru 6d in Appendix D).

Drop-size distribution for samples taken (figs. 2.3 through 2.7) (see Appendix A for Error Analysis) at 0 hours show an unmistakable trend that there is a larger proportion of smaller drops than larger drops. In other words, there is a maxima for the drop size distribution at the lower end of the spectrum. When the emulsion is allowed to stand over a period of time the drops tend to coalesce and the maxima tends to move towards the right.

The drop-size distribution when dispersant is used changes markedly from what it is when dispersant is not used. Figs. 2.3 through 2.7 show the distributions for different shear rates with and without dispersant. When dispersant is present, the distribution does not appear to change significantly with power input. However, when dispersant is not used there is a discernable difference in the distribution. It can be seen that the maxima for the distribution when dispersant is present is less than the maxima when dispersant is not used. This could be attributed to the lower interfacial tension between the oil and water when a surface active agent is used (see table in Appendix B).

If we consider the arithmetic mean of the drop sizes at 0 hours (figs. 2.8 thru 2.13) it can be seen that for a given rpm there was little or no difference between drop sizes at various positions in the tank. This is a corollary to the fact that while the impeller is rotating the forces induced on the drops by the forced circulation is far greater than gravity and the buoyant forces that otherwise would be dominant, when there is no such forced circulation.

In studying the drop size distribution, various averages are used. The number average mean is an obvious choice as it gives appropriate weight for drops of a given size. The weighted mean is given by,

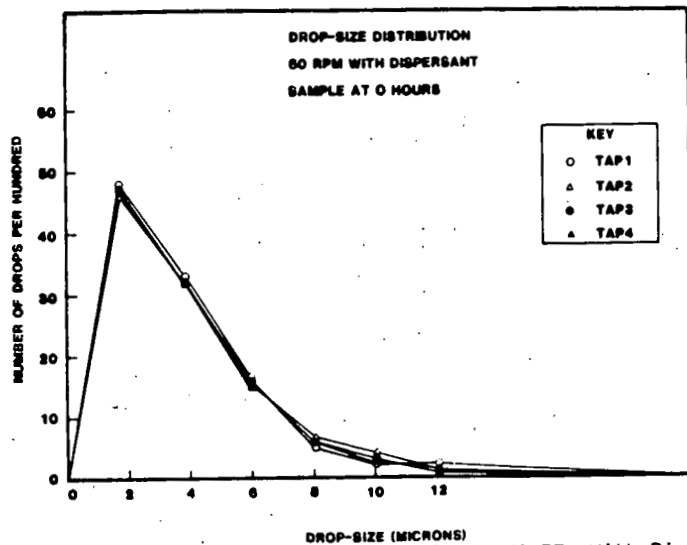


Figure 2.3 Drop-Size Distribution - 60 RPM With Dispersant

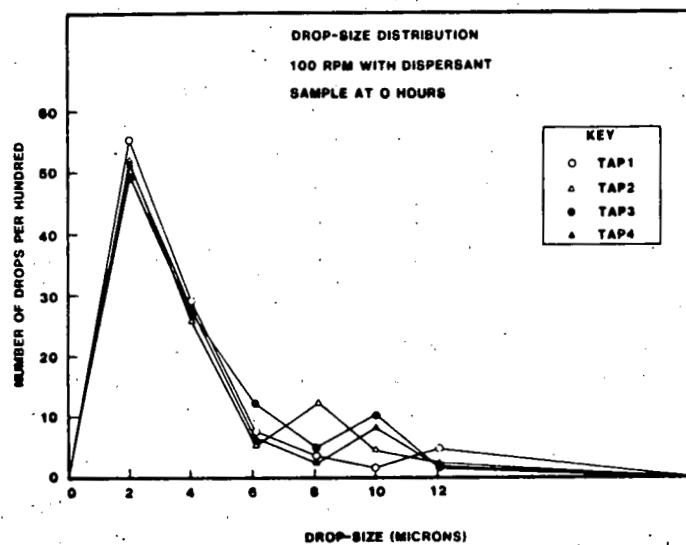


Figure 2.4 Drop-Size Distribution - 100 RPM With Dispersant

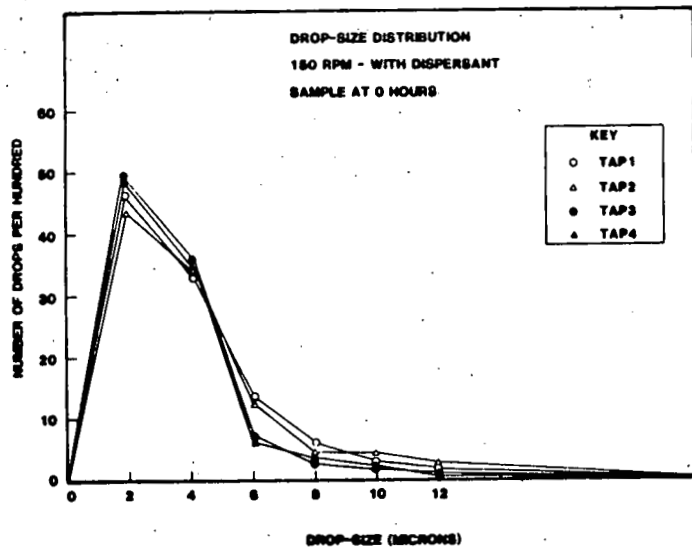


Figure 2.5 Drop-Size Distribution - 150 RPM With Dispersant

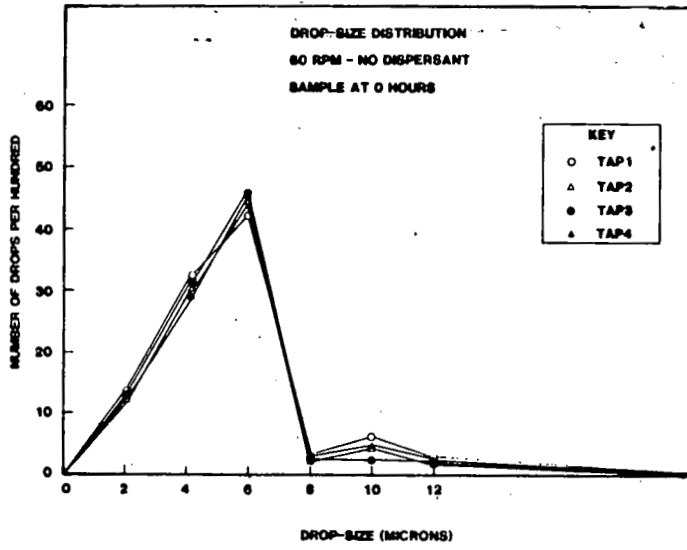


Figure 2.6 Drop Size Distribution - 60 RPM - No Dispersant

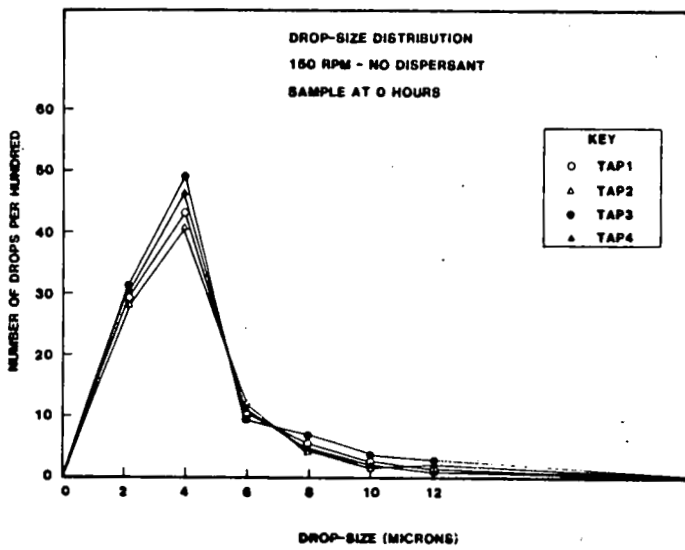


Figure 2.7 Drop Size Distribution - 150 RPM - No Dispersant

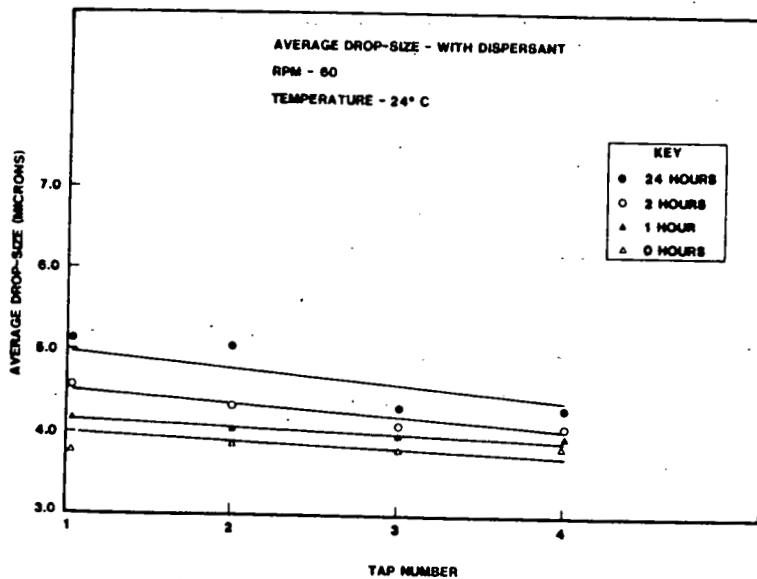


Figure 2.8 Average Drop-Size - With Dispersant RPM -60 - Temperature - 24°C

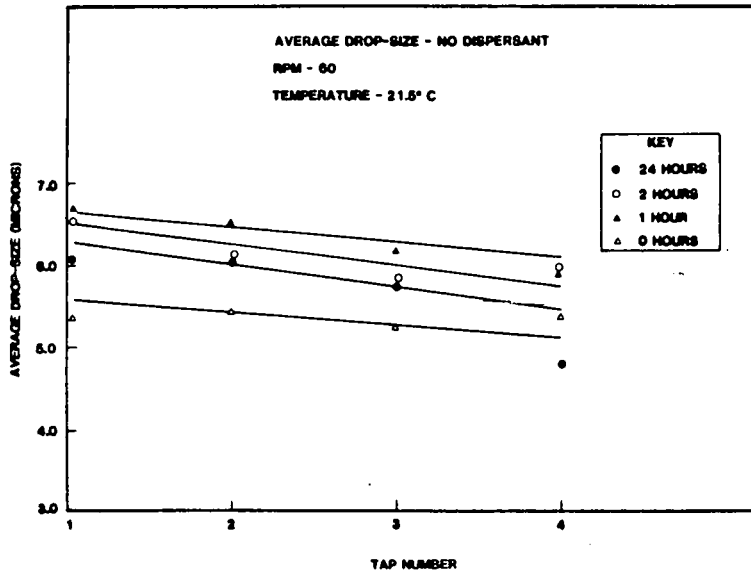


Figure 2.9 Average Drop-Size - No Dispersant RPM - 60 Temperature - 21.5°C

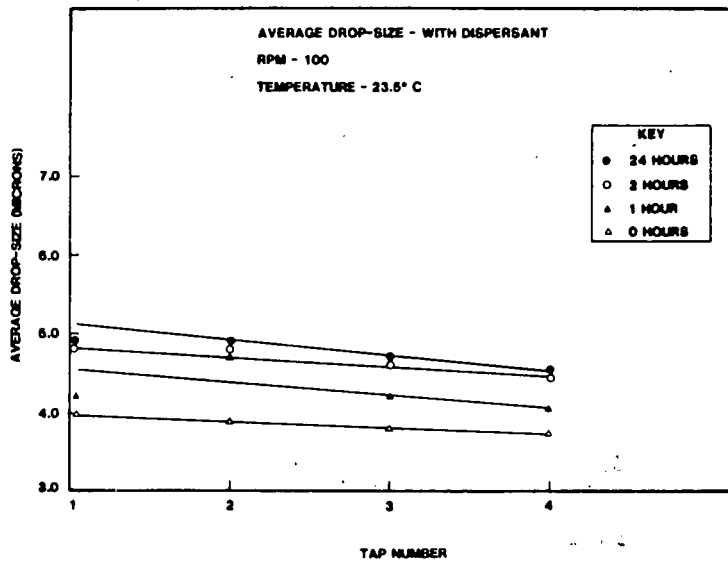


Figure 2.10 Average Drop Size - With Dispersant RPM - 100 Temperature - 23.5°C

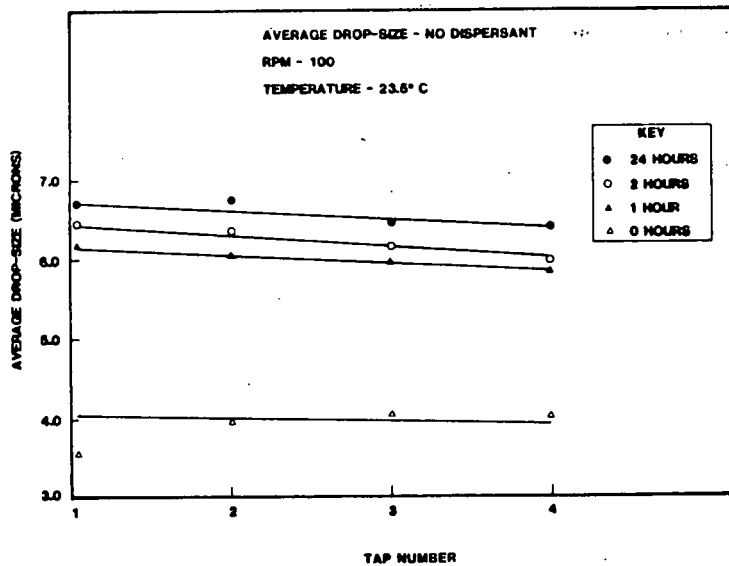


Figure 2.11 Average Drop Size - No Dispersant RPM - 100 Temperature - 23.5°C

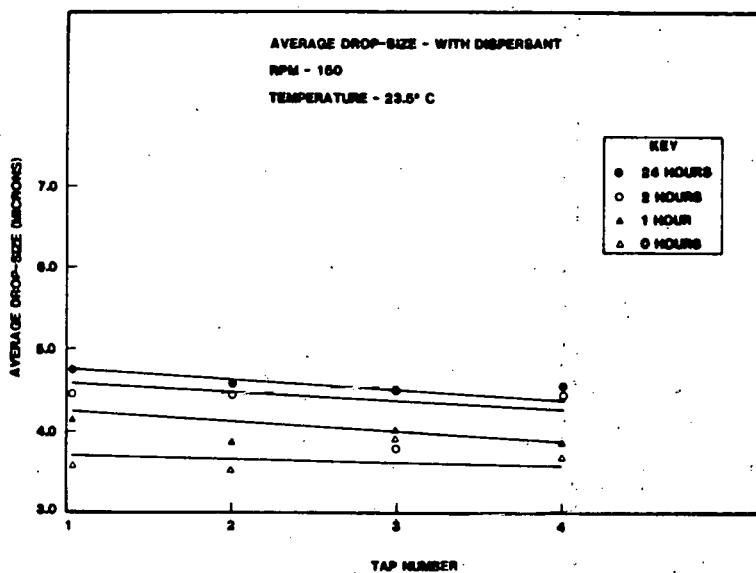


Figure 2.12 Average Drop-Size - With Dispersant RPM - 150 Temperature - 23.50C

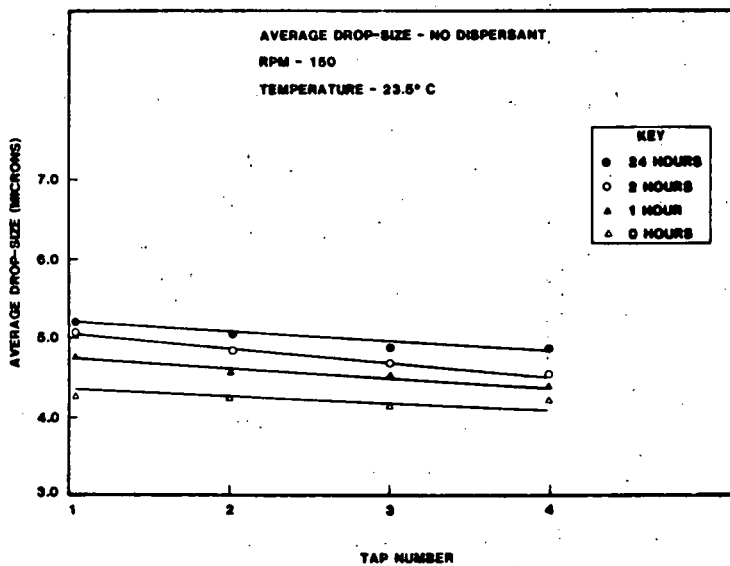


Figure 2.13 Average Drop Size - No Dispersant, RPM - 150, Temperature - 23.50C

$$AM = \frac{\sum N_i d_i}{\sum N_i}$$

While studying interfacial area Sauter Mean is the best choice. Sauter mean is given by

$$SM = \frac{\sum N_i d_i^3}{\sum N_i d_i^2}$$

The drop size distributions show that the average drop size is a function of the rate of shear and interfacial tension. It is seen that we get a finer dispersion when a dispersant is added.

The average drop size at 0 hours is approximately 20 percent smaller when the speed of the impeller was increased from 60 to 150 rpm when no dispersant was present, as shown in figs. 2.9 and 2.13. If the rate of shear is taken to be proportional to the tip speed of the impeller then this represents a decrease in drop size of 20 percent for an increase in shear rate by a factor of 2. In the presence of the dispersant the average drop size for the above two cases was smaller and the difference in drop size was only approximately 3 percent (figs. 2.8 to 2.13).

It was seen that the average drop size (except at 0 hours) increases with time as well as position in the tank as measured from the bottom of the tank. Since in the present investigation the droplets are made up of an incompressible fluid, different vertical positions (and hence the hydrostatic pressure) does not have any effect on their size. Thus the increase in size with time and position are due to coalescence processes taking place. However, coalescence in a system of as small a hold-up as this is bound to be small.

Consider two drops of equal diameters. When they collide and coalesce their combined volumes will be twice the volume of the original drop and the diameter will be 26 percent larger. If the average drop size at the top and bottom levels in the tank are considered at 0 hours and 24 hours (figs. 2.7 to 2.14) it can be seen that the drop size has increased from bottom to top by less than 20 percent only. This shows that coalescence was not a major factor in the instability of the system. This is as should be expected in view of the extremely small hold-up. For the hold-up used in the experiments, and for an average drop size of 4 microns, the mean free path is about 63.3 microns. This means that if the movement of the drops is completely random, the drop will have to travel 15 drop diameters before colliding with another drop. Since Brownian movement which contributes to considerable random lateral movement (in contrast with straight upward movement due to buoyancy) is negligible at drop diameters greater than 0.1 microns (30). The only possible way in which drops could collide is when they rise upwards. This type of collision is bound to be small in systems of small hold-up. This accounts for the fact that the drop-size distribution itself does not vary appreciably with time.

2.4.2 Hold-up and Interfacial Area

Hold-up is defined as the fraction of the dispersed phase in the continuous phase. When dealing with a small hold-up as in the present case, alternate units are used. In this investigation milligrams per liter was found to be a convenient unit.

There was little variation in the hold-up (with respect to different positions in the tank) at the instant the impeller was stopped (figs. 2.14 thru 19). Thereafter, the hold-up decreased continuously with time as well as position, as measured from the bottom of the tank upward. As coalescence in systems of small hold-up are small, the decrease in hold-up is a function of the terminal velocity of the droplet (Brownian movement of droplets of size larger than 1 micron being negligible). At 24 hours, the hold-up was the same for all taps and all rpms with dispersant. This was found to be the case when no dispersant was used also.

Thus the stability of a dispersion of small hold-up will depend to a large extent upon the rate of rise of a drop. If we equate the forces acting on a droplet we get (36)

$$F = \frac{4}{3}\pi R^3 \rho_c g + 2\pi\mu R v_\infty + 4\pi\mu R v_\infty$$

where the first term on the right is the buoyancy force, the second term is the form drag and the third term is the friction drag. When these forces are balanced by the gravitational forces, the drop will rise at a uniform velocity. Thus we have:

$$\frac{4}{3}\pi R^3 \rho_d g = \frac{4}{3}\pi R^3 \rho_c g + 2\pi\mu R v_\infty + 4\pi\mu R v_\infty$$

Solving for the velocity gives,

$$v_\infty = \frac{2}{9} \frac{R^2 g}{\mu} (\rho_d - \rho_c)$$

Thus a smaller drop tends to have a smaller terminal velocity.

If the shearing action of the continuous phase on the dispersed phase accounts for the break up of the dispersed phase, then the shear rate as given by the tip speed of the impeller should have a functional relation to the drop size and thereby to the hold-up. Moreover, a system of lower interfacial tension is inherently more stable thermodynamically, as the work done in creating interfacial area is smaller and hence the potential energy of the system is smaller.

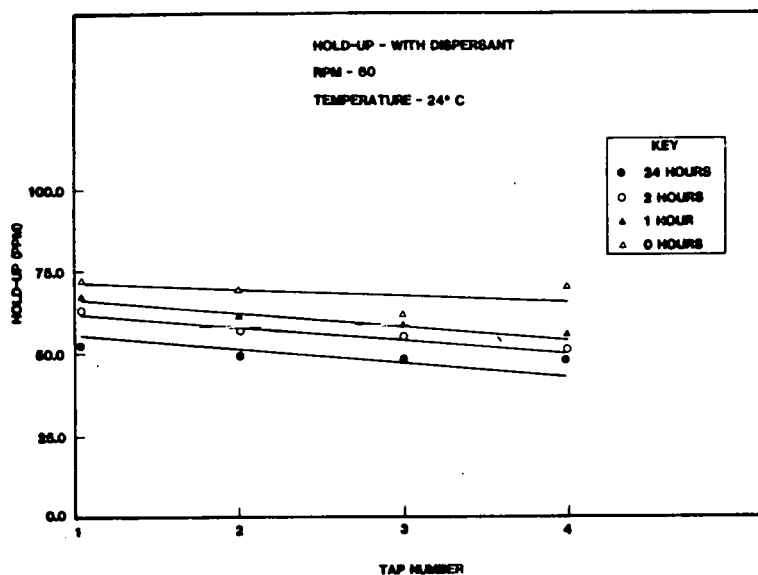


Figure 2.14 Hold-Up - With Dispersant, RPM 60, Temperature - 24°C

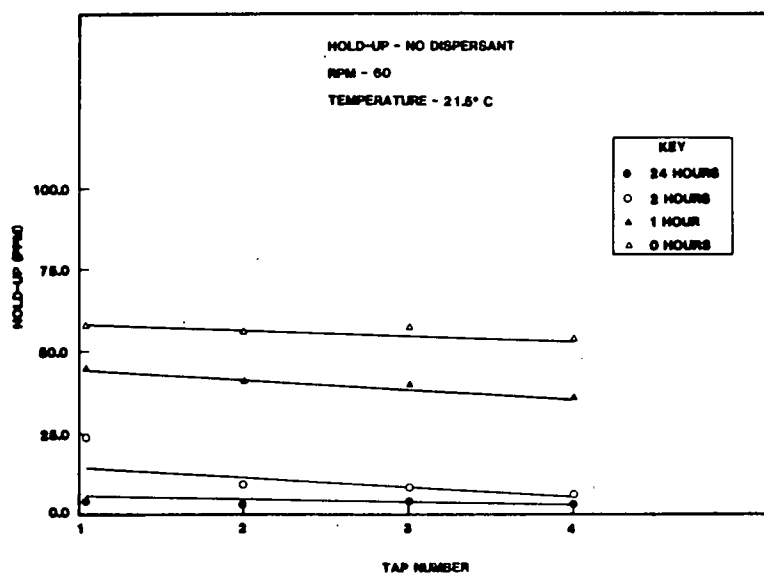


Figure 2.15 Hold-Up - No Dispersant, RPM - 60, Temperature - 21.5°C

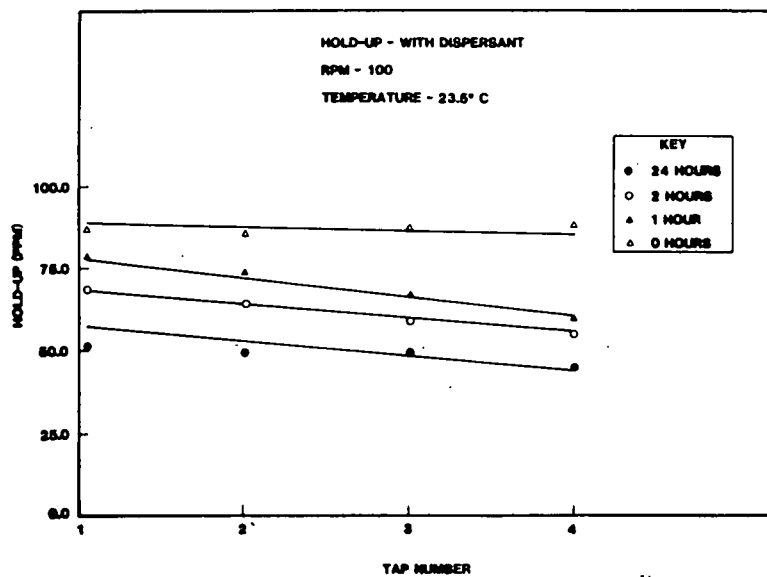


Figure 2.16 Hold-Up - With Dispersant; RPM - 100, Temperature 23.5°C

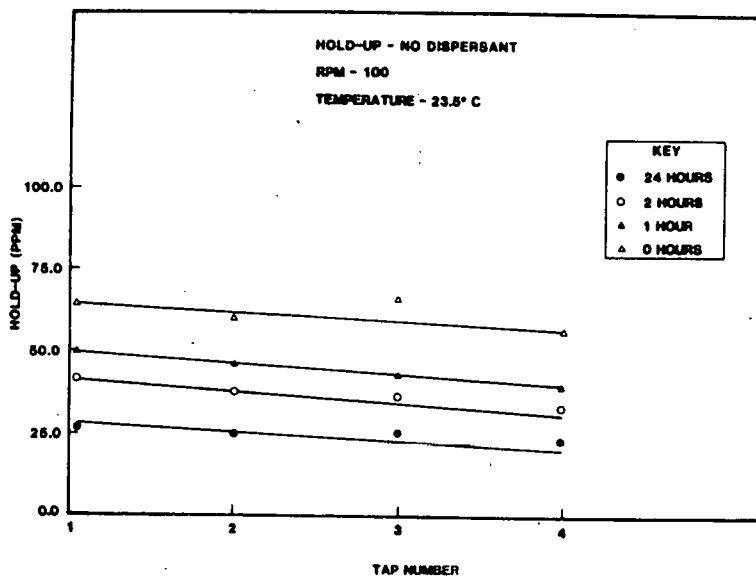


Figure 2.17 Hold-Up - No Dispersant, RPM - 100, Temperature - 23.5°C

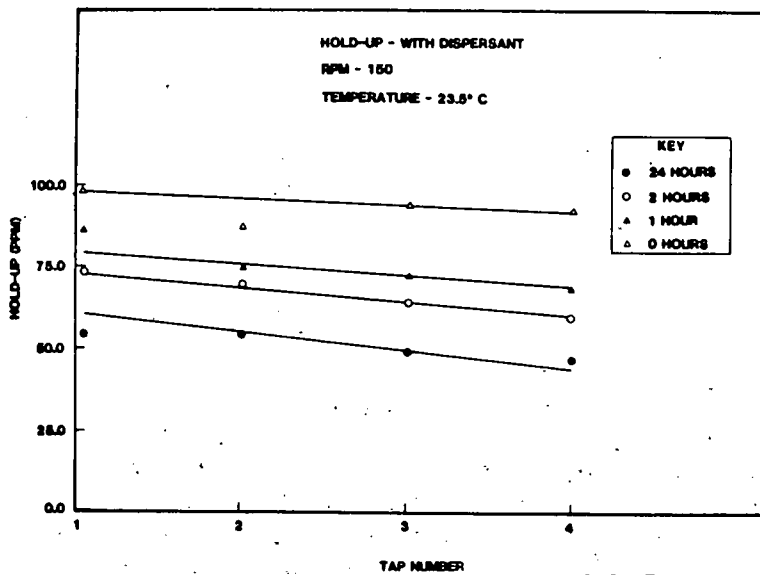


Figure 2.18 Hold-Up - With Dispersant, RPM - 150, Temperature - 23.5°C

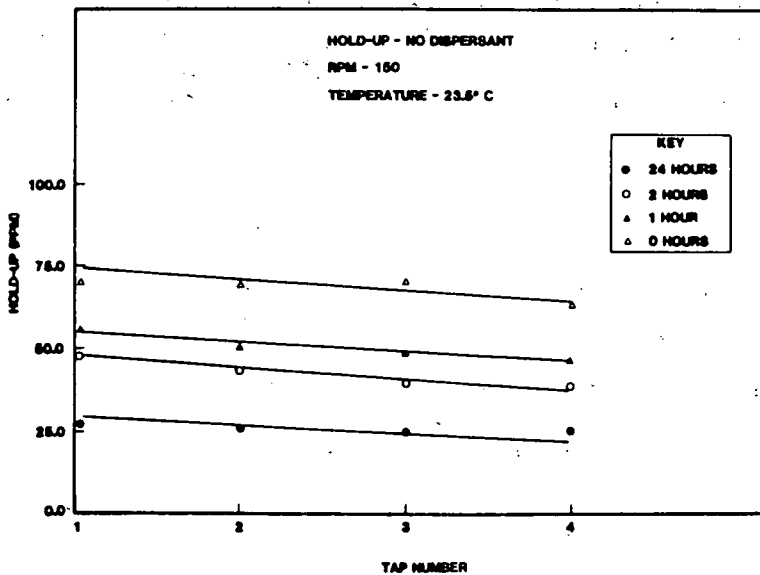


Figure 2.19 Hold-Up - No Dispersant, RPM - 150, Temperature 23.5°C

An analysis of the hold-up data shows that the hold-up when no dispersant was used, for samples taken at 24 hours was approximately constant and was very close to the solubility limit of crude oils usually observed (figs. 2.14 thru 19). When the dispersant was used, the hold-up at 24 hours was approximately constant but was higher (by a factor of approximately two) than the hold-up at 24 hours. This makes a good case for the use of dispersants in dispersing oil spills, if hold-up is the only criteria. As the dispersed phase was of lower density than the continuous phase, it naturally rises upward, and therefore the variation of the hold-up with time showed that the hold-up increased with height as measured from the bottom of the tank.

Specific interfacial area is a function of the hold-up as well as the Sauter Mean diameter of the drops. The interfacial area is given by,

$$A = \frac{6 \times \phi}{SM}$$

As had been mentioned earlier, in systems of small hold-up like the one used in these investigations, coalescence is negligible and therefore the variation in the Sauter Mean diameter with height as well as time was not great. Therefore, the interfacial area showed (figs. 2.20-25) a variation which was similar to that shown by the hold-up. As the hold-up in the case where dispersant was used was higher, so was the interfacial area.

The fraction of the oil which was initially added to the system that goes into the water column is a function of the interfacial tension, and the rate of shear (or rpm). In the series of experiments, the largest fraction of oil that went into the water column when no dispersant was used was only 61 percent at 150 rpm, as against 86 percent at the same rpm when dispersant was used. The higher intake of hydrocarbons with the application of dispersant could be due to increased stability of the dispersion and the formation of sub-micron droplets (this appears to be valid apart from the effects of the lower interfacial tension and variations of other physical properties). The hold-up of the oil at 24 hours is possibly the best indication of this increased 'solubility', which was higher by almost a factor of 2 when the dispersant was used. Since there is no sharp dividing line between 'true solubility' and sub-micron dispersibility, it is hard to say which of the two was predominant at the conditions cited above (17).

In the experiments in which a temperature of 10⁰ C was used (see table 2.9-12), the interfacial tension between the oil phase and the aqueous phase was 3.91 dynes/cm, in the presence of the dispersant. The interfacial tension at the same temperature and when no dispersant was used was found to be 25.1 dynes/cm (see table in Appendix B). The variation in hold-up and average drop size followed a trend that was very similar to that which was observed for the runs at the higher temperature. The hold-up, and consequently the interfacial area (after having been normalized to make allowance for the smaller tank), was found to be lower than that for the runs at higher temperature. Thus the effect of the lower temperature was to give a dispersion that was less stable

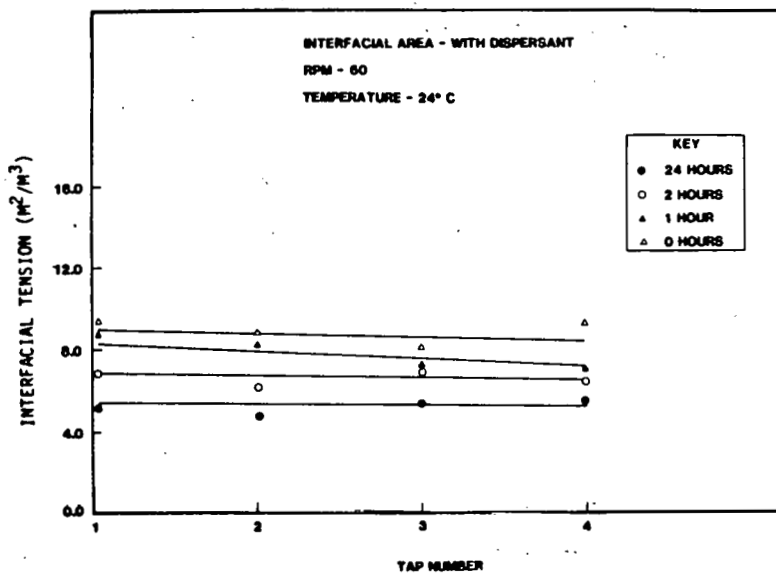


Figure 2.20 Interfacial Area - With Dispersant, RPM - 60, Temperature - 24°C

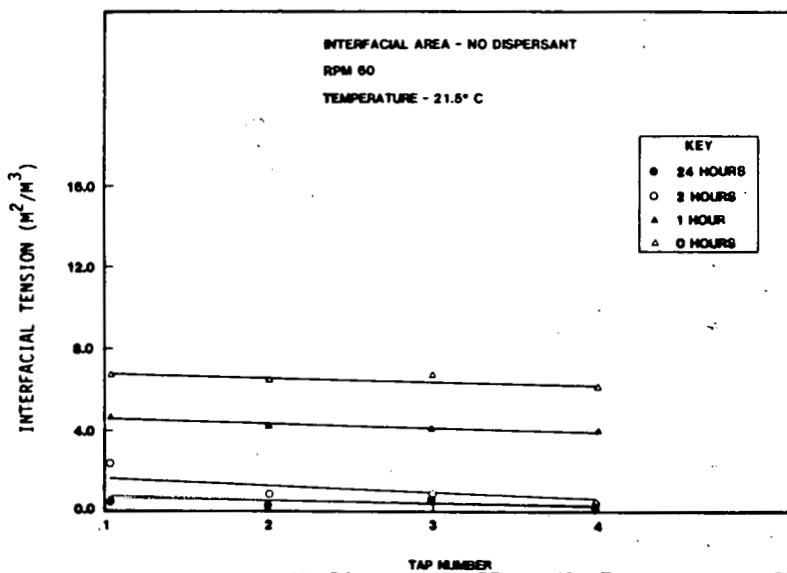


Figure 2.21 Interfacial Area - No Dispersant, RPM - 60, Temperature - 21.5°C

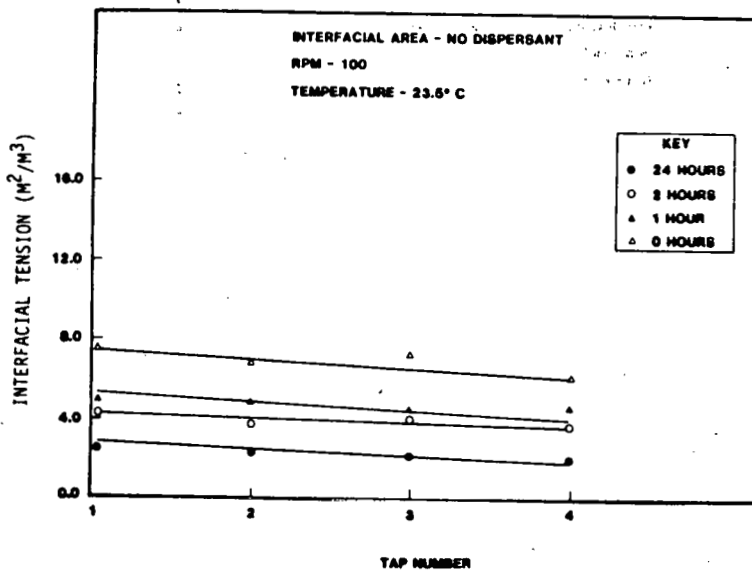


Figure 2.22 Interfacial Area - No Dispersant, RPM - 100, Temperature - 23.5°C

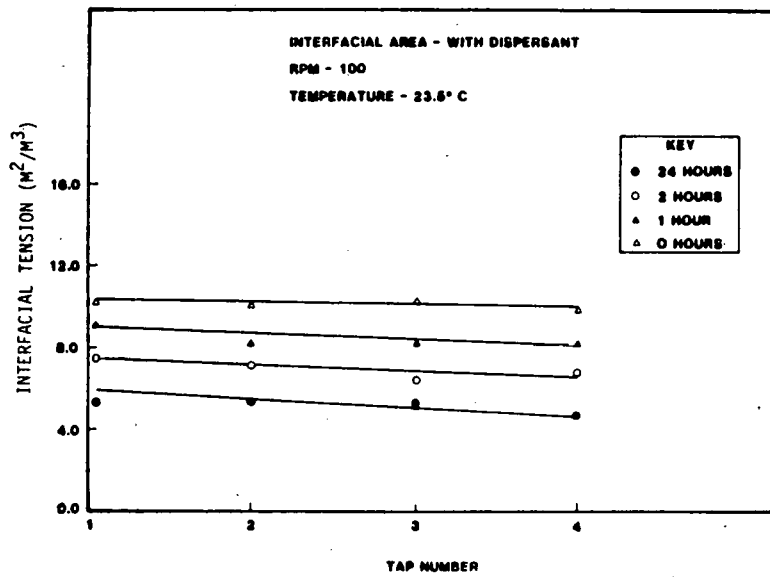


Figure 2.23 Interfacial Area - With Dispersant, RPM - 100, Temperature 23.5°C

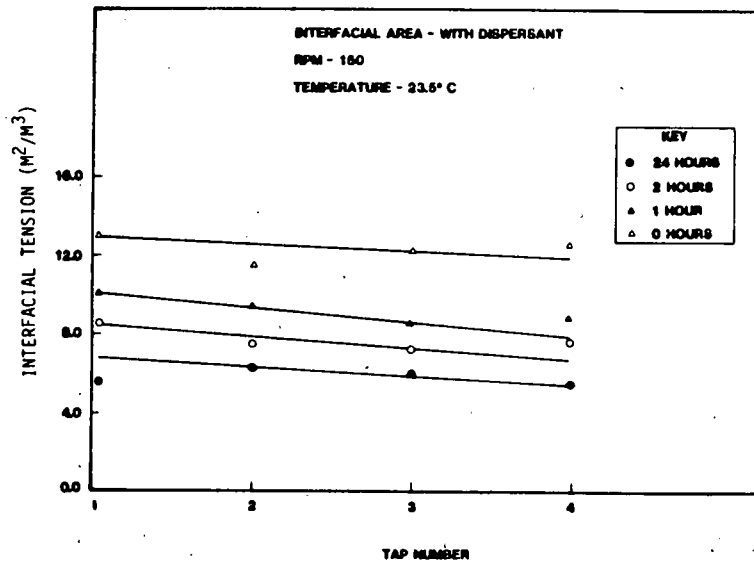


Figure 2.24 Interfacial Area - With Dispersant, RPM - 150, Temperature 23.5°C

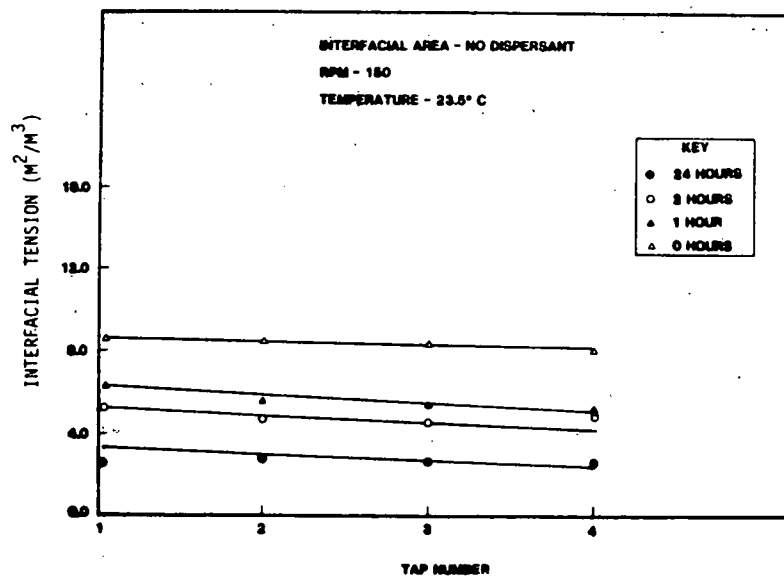


Figure 2.25 Interfacial Area - No Dispersant, RPM - 150, Temperature 23.5°C

because of the higher interfacial tension.

In contrast to the runs at 10⁰ C, the runs at room temperature varied over a range of 2.5⁰ C. Over the range of 5⁰ C to 22⁰ C, the interfacial tension varied by approximately 8.0 dynes/cm. Assuming that the interfacial tension is a linear function of temperature over this temperature range, it can be seen that the variation of the interfacial tension over a range of 2.5 C is only about 1 dyne/cm. The effect of this variation of the interfacial tension over such factors as work done and power input is only about 10.0 percent. Since the drop-size is proportional to a fractional power of the interfacial tension (32), the variation of the drop-sizes due to variation in the ambient temperature is bound to be only less than 10.0 percent.

It had been observed that hydrocarbons could enter the water column without any power input. This is indicated by the runs at 0 rpm - i.e., no power input. Though the hold-up was not as large as was the case when the impeller was used, it was considerable in view of the fact that there was no power input involved.

When two phases are brought into contact with each other, initially the chemical potentials of the various components in each phase are not equal and therefore this sets up a potential difference for the components between the phases. Thermodynamically, when there is a potential difference, the tendency is to equalize them. This is achieved by the diffusion of the components from the phase in which they have higher potentials to the phase in which they have lower potentials. The diffusion continues to take place until all chemical potentials have been equalized. Once the different components are in the second phase, they may tend to agglomerate and form droplets or micelles.

Thermodynamic potential is defined as:

$$\mu_i = \left(\frac{\partial G}{\partial n_i} \right)_{T, P, n_j}$$

where G is the Gibbs free energy, n the number of moles of the constituent j, T and P temperature and pressure respectively (39). For phase A and B the Gibbs criteria for equilibrium is:

$$\mu_i^A = \mu_i^B$$

The chemical potentials are very difficult to use for studies involving crude oil in view of the large number of components involved. Phase equilibria involving more than three or four components are seldom solved by using thermodynamic potentials.

In this context it could be asked, what is the role played by power input in dispersing the crude in the water column? The thermodynamic potential; as it provides the driving force should have been sufficient to do the dispersion. But dispersion of one component into another takes

place through the interface between the phases, and the rotating impeller by breaking up the dispersed phase provides a larger interfacial area, thereby speeding up the equilibrium process. The rates at which equilibrium could be achieved when no power input is involved also depends on the interfacial resistances involved. It is difficult to compare the two methods (with power input and without power input) as little is known of the interfacial resistances. However, power input has one beneficial effect. The mass transfer rate between an oil slick and the water column is proportional to the concentration difference. The forced convection currents due to power input helps keep this concentration difference high thereby increasing the rate of mass transfer.

The mechanical work that is done in creating new surface area is given by the product of the interfacial tension and the new surface area created. It can be seen that the fraction of the total energy input that goes into making new surface area is of the order of 10 percent (Appendix C). Apart from the fact that the impeller action for creating new surface area (or small droplets) is therefore very inefficient, it also shows that one should treat with great caution the use of power input as a basis for determining the creation of new surface area and hold-up.

2.5 Conclusions and Recommendations

The basic question posed in this investigation was whether it was desirable to use a dispersant for emulsifying crude oil for later biodegradation.

The series of experiments conducted show that crude oil can be effectively dispersed using a commercial dispersant, Corexit 9527 without excessive power input. (Large power input was considered impractical in an oil-spill situation on the high seas.) The interfacial area and the hold-up, which are the important parameters when considering biodegradation was found to be 2-3 times that when no dispersant was used. In this context it is important to remember that not all dispersants are useful for the purpose of biodegradation.

It was found that oil could enter the water column even when there was no power input. This is significant in that given sufficient amount of time, the oil could be effectively made to enter the water column without any power input - a desirable situation in a million gallon oil-spill.

The drop size distribution found for the 1-12 micron range can be considered to be truly representative of the emulsion. Further, this range of droplets is all that is necessary to study the emulsification process and the stability of oil-in-water emulsions.

It was observed that coalescence in a system of such a small hold-up as parts per million is very small. Therefore the instability of the system is due to the upward movement of the droplets in the continuous phase. This movement becomes ever smaller as the drop diameters become

smaller.

It is hoped that it will be possible to translate the experimental data at the higher temperatures to actual field conditions at much lower temperatures. Interfacial tension is the most dominant factor that is affected by the temperature. A decrease in the temperature from 22 C to 5 C increases the interfacial tension approximately by a factor of 2 to 3. Since the work done and consequently the power input is a linear function of temperature, it is expected that an increase in interfacial tension by a factor of 1.1 would call for an increase in the power input by the same factor.

The following recommendations are made:

i) To establish a base line for studying dispersibility of crude oils in water, pure hydrocarbons should be used.

The experiments conducted with Kuwait crude will not give much information where another crude is involved. This is primarily because the crudes themselves contain many surface active agents in the form of hydrocarbons with hydroxyl and carbonyl groups. The proportion of these vary widely from crude to crude.

ii) More efforts should be made to study the effect of dispersants in dispersing oil spills without input of power.

iii) Since the stability of the dispersion is desirable the idea of stabilizing the dispersion with finely divided solids should be investigated. Use of solids would mitigate the toxic effects of most common dispersants.

The temperature on the high seas in an actual oil spill situation could very well be close to the freezing point on a winter day. Therefore, the problem of correlating the experimental data at the higher temperatures to lower temperatures in the ocean naturally arises. On the basis of the effect of temperature on viscosity and interfacial tension, it can be estimated that the interfacial area will be smaller by approximately 10-15 percent.

3.0 The Effect of Wind and Wave Motion on Oil Entrainment

Rodger B. Dowdell

Steven G. Parks

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3.1. Introduction

The wind-wave tank experiment is part of a larger study conducted at the University of Rhode Island to assess the environmental impact of treated and untreated oil spills. To develop a comprehensive model for oil slick impacts, this study required information about the amount of oil that would be dispersed under the ocean surface in a given sea state. It is believed that the largest oil concentrations result from dispersed oil droplets and that wave motion and the turbulence from breaking waves are an important dispersive mechanism. In addition, it has been shown that the oil properties can have an important effect on the amount of oil dispersed, and that these properties can change significantly over time. The experiments that have been done to date have provided valuable observations of the processes involved as well as some data. However, it has been difficult to establish even simple correlations between sea state and sub-surface oil concentrations for a number of reasons. The data from accidental spills is incomplete and it is not usually obtained under well documented conditions. Also, it is difficult to simulate sea-like conditions in the laboratory, and there is no simple accurate method available for measuring oil concentrations in water.

The wave tank experiment was proposed to address these problems and to add to the existing data. From the beginning, three design constraints were imposed: i) the experiment must be able to subject a small oil slick to various sea-like conditions, ii) it must be able to operate for an extended period of time, and iii) it must keep the effects of artificial barriers such as tank walls or containment booms to a minimum. This latter constraint is particularly difficult because water waves tend to push floating material in the direction of propagation. To solve these problems, a circular tank was designed and built with a variable speed wave generator around its perimeter, Figures 3.1 and 3.2. Water waves created at the edge of the tank travel toward the center where they interfere and sometimes break. Thus, the floating oil is contained in the region of maximum agitation solely by the wave drift currents, and no barriers are needed. The oil slick can be kept in a field of waves for as long as desired.

Of course this model has limitations. The energy in wind generated ocean waves is distributed over a band of frequencies where the energy concentration and bandwidth is dependent on wind fetch, duration, and water depth. The energy in the mechanically generated waves will be concentrated in a few distinct frequencies depending on the wave generator and tank geometries and the generator frequency. Also, the constructive interference of the waves at the center of the tank causes the waves to become steeper than they appear in the ocean. Currents are induced in the tank by the waves propagating toward the center, and in time these establish a circulation throughout the tank. All these differences are a result of the finite geometry of the experiment combined with a deterministic rather than a random forcing function for the waves. This has to result in a somewhat unsea-like environment. Nevertheless, the waves in the center of the tank have many apparent similarities to wind generated ocean waves.

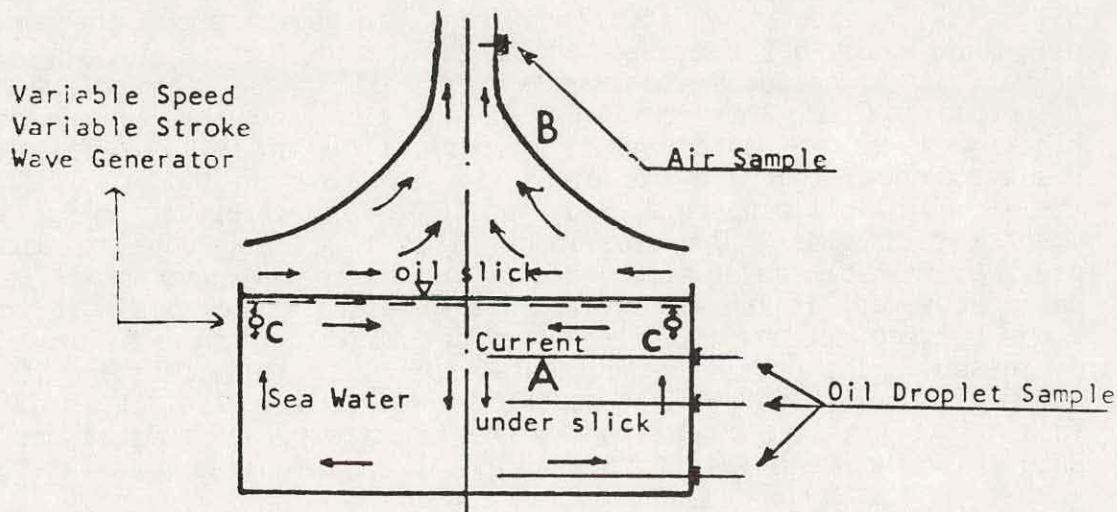


Figure 3.1. The Wind Wave Experiment

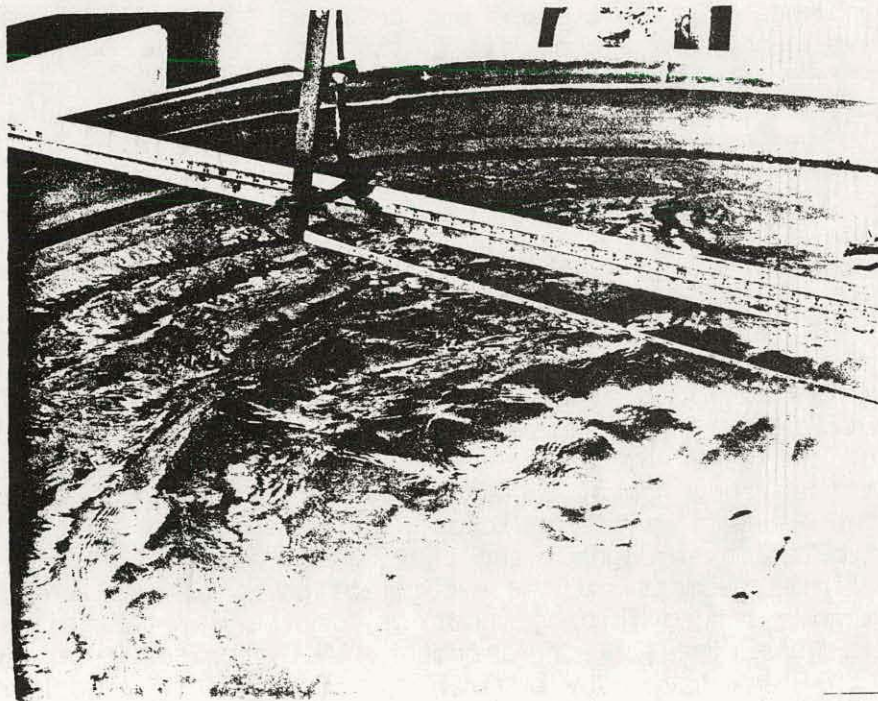


Figure 3.2. Circular Wave Tank

The intent of the experimental test program was to investigate the relationship between the amount of any given oil dispersed into the water column from a slick on the surface, and the macroscopic physical properties of the waves causing the dispersion. Of particular interest were the effects of any oil property changes on the oil in water concentrations as the oil weathers. Consequently, the experiment was designed toward this end. No attempt was made, for example, to perform detailed investigations of the turbulent structure in the breaking waves, or to test for chemical changes in the oil. Rather, a simple function between sea-state and oil concentration was assumed to exist. The major effort was devoted to measuring the important parameters that would be included in this function such as the oil concentrations in the tank, and the wave parameters including an estimate of the frequency and extent of wave breaking. Other parameters that were deemed peculiar to the experiment, such as the induced water currents, that might affect any generalizations from the data were also measured. Oil properties and water properties were only measured to establish baselines and were not investigated for changes. The presumed function is certainly an approximation which ignores many components of the problem. However, the observations and data suggest that this assumption may be valid.

3.2. Experimental Apparatus

All of the oil dispersion experiments for this investigation were conducted in the circular wave tank shown in Figures 3.1 and 3.2. This tank is 3 feet high, 8.1 feet in diameter, and has a nominal capacity of 1000 gallons. A 24 by 36 inch plexiglass window was installed in the side of the tank to permit observation of subsurface phenomena. The waves were created by an 8 foot diameter circular hoop mounted concentrically inside the tank. The hoop, shown in Figures 3.1. and 3.2., is constructed of 1 inch diameter aluminum rod and fastened to the tank with 4 aluminum connecting arms. The wave generator is driven by a slider crank mechanism attached to a Dayton variable speed 1/2 HP gear motor (model No. 3n259) which can be adjusted to operate at any frequency between 18 and 130 cycles per second.

A hood is placed over the surface of the tank and connected to the suction side of two 5 HP, two speed blowers. The air flow over the surface is in a radial direction and has an approximately constant velocity, which can be varied from about 10 knots to 25 knots. The wave motion can be created by the wind alone, the wave maker alone, or both in combination. A wide variety of wind-wave conditions can be created.

When the wave generating hoop is adjusted to pierce the water surface during an oscillation, waves are created that travel towards the center of the tank, interfere, and may break. These waves induce surface currents directed radially inward which confine any floating oil to the region in the center of the tank where it is constantly exposed to the waves and dispersed under the surface. Preliminary experiments and analysis of the wave motion in the tank showed that there are many resonant modes of the water in the tank in the frequency range of the wave-maker. If the wave generator was at or near a resonant frequency, large waves develop in the tank and sometimes a large seiching motion (Wavelength 2 D) was established. Thus, it was necessary to experiment by trial and error with different combinations of generator frequencies,

generator amplitudes, and water depths until satisfactory wave patterns were found that did not change significantly over time. Eventually, it was decided to operate the wavemaker at 1.33 and 2.13 cycles per second with a water depth of 27.75 inches. With this depth restriction, the capacity of the tank is 890 gallons (3470 liters). The vertical location of the wave generating hoop was adjusted so that at the top of its stroke 1/4 of the diameter of the bar was below the still water level. The amplitude of the oscillations was kept constant at 1.5 inches throughout all the tests.

Because this dispersion experiment requires the measurement of very low concentrations of oil in water, extreme care was taken throughout the design and construction of the test apparatus to use materials that were chemically inert and easy to clean. The wave tank was constructed from wood and coated on the inside with 4 layers of a polyester resin which had been shown not to leach any detectable levels of contaminants into the water. The wave generating apparatus was made completely out of teflon and aluminum.

The measurement apparatus that was used included equipment for determining wave heights, water current velocities, water and oil properties, and oil concentrations. The wave measurements were performed with two Coastal Data Service model WS 100 capacitive wave staffs. These instruments were specially modified to increase their sensitivity by replacing the coated metal probes that were supplied with the instrument with 16 gauge teflon coated wire. The voltage time series produced by the probes were recorded on magnetic tape with a Hewlett Packard 3960 FM tape recorder and later digitized using a Nova 1200 mini-computer.

Rhodamine B dye was used to determine the water current velocities. Samples taken from various tank locations at uniform time intervals were analyzed for fluorescence (dye concentration) with a Turner model 111 fluorometer. The water and oil interfacial and surface tensions were determined with a Cenco-Dunouy 7045 Tensiomat. This instrument measures the interfacial tension by balancing the force required to pull a platinum ring through the fluid interface against torsion in a fine calibrated wire. The tension values are recorded directly from the instrument and corrected for force imbalances in the system as instructed in the manual.

Specific gravities were calculated by weighing an accurate volume of fluid in a siphonometer on an analytic balance. Water and air temperatures were measured with standard laboratory mercury thermometers. Photographs of each experiment were taken with a Mamiya 35 mm SLR camera. In addition overhead still photos were taken at 5 to 10 second intervals with a Sanyo Super 8 mm movie camera. A complete description of the apparatus used to determine the oil in water concentrations will be given in the description of the sample analysis procedure.

The entire experimental set-up was located in a shed adjacent to Narragansett Bay. The experiments were performed at ambient temperatures using both bay water and fresh water. The water used in the latter experiments was passed through three filters to remove all particles larger than 5 microns. Care was taken to fill the tanks with sea water close to high tide to minimize any contaminants coming from Narragansett Bay.

3.3. Experimental Procedure.

The test procedures that were followed throughout the experimental program are described in the following sections. Ten experiments to measure the oil in water concentrations resulting from the wave action in the tank were performed using the standard experimental and sample analysis procedures listed. Three input conditions; wave generator frequency, oil volume, and water type (fresh or sea water) were varied. Most of the sea water tests were duplicated. Care was taken to insure that the experimental and chemical analysis procedures were exactly the same for all the tests with one exception: the water sampling times were changed when it became apparent that the sample variability and oil dispersion time scales were not what was originally expected. This is described completely in the sampling procedure description below. A complete list of the test conditions for each experiment is given in Table 3.1.

The input conditions (wave height, length, frequency and water current velocities and directions) caused by the wave generator were measured independently of the oil dispersion experiments. Ideally, a complete experiment would measure the oil concentrations and the wave and current conditions in the tank simultaneously. Unfortunately, oil on the water surface complicates things considerably. There are presently no readily available instruments for measuring wave heights and current velocities that will work in the presence of oil. In addition, any instrument placed in the wave field at the center of the tank would have an unknown effect on the dispersion process. Rather than develop special instrumentation it was decided to perform the wave and current measurements separately. This cannot be accomplished without some error. Oil has a visible effect on water waves. It tends to damp out high frequency capillary waves and inhibit the breaking process so that the waves become slightly steeper before collapsing. However, because the size of the experimental slick is small, and the wave action at the center of the tank was intense, it was felt that any change in the wave field due to the presence of an oil slick would be minimal, or at least that it would not be detectable within the accuracy of the experiment. This was later confirmed, in part, through observations and comparisons of photographs.

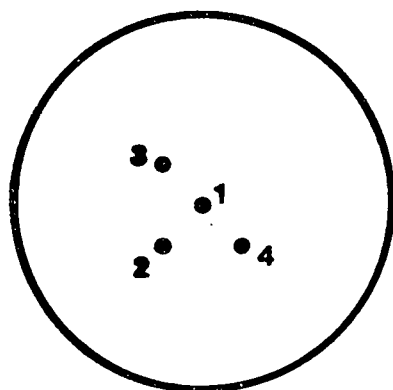
3.3.1. Wave Measurements

Wave data time series were obtained for both the 1.33 and 2.13 cycle per second wave generator frequencies. Data were obtained from the capacitive wave probe locations shown in Figures 3.3 and 3.4. (Note: the radii listed in the figures are referenced to the centerline of the generating hoop.) These locations were chosen to measure the wave parameters at the point of maximum observed wave activity, (tank center) and at the locations where turbulent breakdown of the regular wavefronts was just perceptible. Locations at equal radii were chosen to check for symmetric conditions in the tank.

Two capacitive wave staffs were available and consequently the data were recorded in pairs. Before and after each recording, a calibration record was established by measuring simulated water level changes in the tank. Each instrument was raised and lowered 12 cm relative to the water surface along a vertical carriage. Their output was recorded at 2 cm

TABLE 3.1 -SUMMARY OF EXPERIMENTAL CONDITIONS
AND PROPERTY MEASUREMENTS

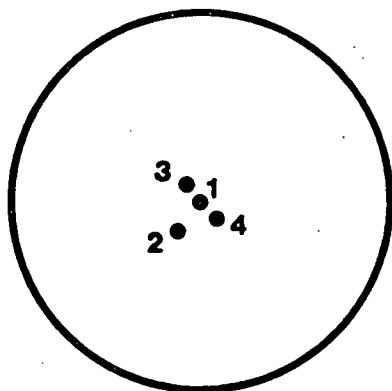
Experiment	1	2	3	4	5	6	7	8	9	10
Date	2-21-79	3-3-79	6-13-79	6-26-79	6-28-79	7-10-79	7-12-79	7-15-79	7-31-79	8-3-79
Water type	Fresh	Fresh	Salt	Salt	Fresh	Salt	Salt	Salt	Salt	Salt
Water Specific Gravity	1.00	1.00	NA	1.021	1.00	1.023	1.024	1.024	1.023	1.022
Water Temperature Range:										
Minimum Temp °C	5	5.5	15	18	18	22	20	20	25	24
Maximum Temp °C	8	6	16	20	20	23	22	22	27	26
Water Salinity ‰	NA	NA	NA	NA	NA	29.8	29.8	30.2	NA	NA
Ambient Air Temperature Range										
Minimum Temp °C	5	6	15	17	18	20	22	21	27	27
Maximum Temp °C	9	8	16	26	22	24	24	23	31	29
Amount of Kuwait Crude Oil Added (ml)	60	60	60	60	60	60	120	120	60	60
Interfacial Tension Measurements (dynes/cm)										
water-air	75.5	75.5	NA	69.7	71.4	71.6	69.3	68.8	NA	NA
oil-air	50.9	50.9	NA	26.9	26.5	26.3	26.3	26.1	NA	NA
oil-water	26.6	26.6	NA	20.1	26.2	20.0	20.3	20.4	NA	NA
Measurement Ambient Temperature °C	est 8	est 8	NA	22	22	26	26	26	NA	NA
Wave Generator Frequency (cycles/sec)	1.33	2.13	1.33	2.13	2.13	1.33	2.13	2.13	1.33	1.33



- 1 - Tank Center
- 2 - 36cm Radius
- 3 - 36cm Radius
- 4 - 36cm Radius

FIGURE 3.3

WAVE PROBE LOCATIONS GENERATOR FREQUENCY 1.33



- 1 - Tank Center
- 2 - 25cm Radius
- 3 - 13cm Radius
- 4 - 13cm Radius

FIGURE 3.4

WAVE PROBE LOCATIONS GENERATOR FREQUENCY 2.13

intervals. A slight amount of drift was evident in the instrument outputs due to rundown of the power supply batteries. To obtain the conversion factor from volts to cm the best linear fits obtained from the two sets of data were averaged. Using this technique, output data values are accurate to within 2 percent of reading over a range of plus or minus 12 cm. The wave probe response time was found to be instantaneous if the probe remained clean. However, any water contaminants would increase the response time dramatically, up to a few seconds in some cases. This is a result of water adhering to the probe wires and draining off slowly. To ensure adequate response, the probes were oscillated at known amplitudes while their output was checked on an oscilloscope. These tests were performed before each experiment to insure that the probe readings were not affected by any surface contaminants.

Overhead still photographs and slow motion movies were taken to supplement the data and to further document the wave field. Before the tests the tank was allowed to settle for 1 hour. Any visible debris was either skimmed off the water surface or extracted from the tank. The wave generator was run for 15 minutes to allow conditions in the tank to reach steady-state before any measurements were taken.

To analyze the data for frequency components using fast fourier transforms, the necessary sampling frequencies and recording times were chosen by following the procedure outlined in Bendat and Piersol* (1). A sampling interval $\Delta h = T$ was chosen so that

$$\Delta h = 1/(2f_c) \leq 1/(2f_d) \text{ sec.}$$

where f_c is the Nyquist folding frequency, and f_d is the highest possible frequency expected in the data. If $f_d = 20$ hz (an extremely conservative estimate):

$$\Delta h = 1/2(20) = 0.25 \text{ sec.}$$

To achieve an effective resolution bandwidth B_e of 0.1 hz requires that each sample record be T_r seconds long where

$$T = 1/f = 10 \text{ sec.}$$

Choosing a 512 point record sampled at $\Delta h = 0.025$ seconds gives $T_r = 12.6$ seconds.

The random error is minimized by segment averaging. If the original data is assumed to be Gaussian, the normalized standard random error ϵ_r is given by

$$\epsilon_r = \sqrt{1/q}$$

where q equals the number of ensembles of length T_r . Therefore, if

$$\epsilon_r = .1, q = (1/\epsilon_r)^2 = 100$$

*References denoted by numbers in brackets.

and the total record length T required is:

$$\begin{aligned} T &= qT_r \\ &= 100 (12.6) \text{ sec.} = 21 \text{ min.} \end{aligned}$$

As a result of the foregoing analysis, 25 minute records sampled at 40 hz were obtained for each probe location.

3.3.2. Current Measurements

The surface drift currents created by the water waves propagating toward the tank center induce a subsurface return flow directed radially outward. This circulation could be easily observed by watching the motion of neutrally buoyant particles of debris. Unfortunately, the extremely low flow velocities present precluded the use of conventional instruments to obtain velocity profiles.

Measurement of the average convective circulation velocities were made using Rhodamine dye. Four experiments were performed to measure radial and circumferential water velocities as well as to estimate the time necessary to uniformly mix contaminants throughout the tank. The experimental procedure was as follows: the wave generator was run for one hour to ensure that steady-state conditions had been achieved. Then, 30 ml of Rhodamine B dye which had been diluted to be within 1 percent of the specific gravity of the tank water was applied to the center of the tank. Thirty ml water samples were then taken from the sampling valves located at the edge of the tank. The samples were taken at equally spaced time intervals, the time intervals were varied from experiment to experiment. Dye concentrations were later determined by fluorescence measurements with a Turner model 111 fluorometer. Average current velocities could then be found by computing the time differences between measured concentration peaks.

In addition to these tests, numerous visualization experiments were performed with the dye to further establish the magnitude and direction of the water velocity throughout the tank and to locate any eddies. Also, surface current velocities were measured by timing the travel of 5 cm square paper drifters over the 3 paths shown in Figure 3.33.

3.3.3. OIL CONCENTRATION MEASUREMENTS

The amount of oil dispersed into the water column at any given time was determined by chemically analyzing 0.5 liter water samples taken from three depths under the slick (see Fig. 3.34). To minimize any disturbances to the experiment while tests were underway, the water samples were obtained through 4 foot lengths of 7 mm outside diameter glass tubing fixed to the valves at the edge of the tank. Visualization experiments were conducted to estimate the effect that the tubes would have on the sampled oil-water dispersion. It was found that in all cases the predominant oil droplet diameter was significantly less than the 5 mm inside diameter of the tube. Almost all of the oil droplets ducted through the tube were collected intact. Consequently, the effect of the

glass tubes on the oil concentration in the samples was thought to be minimal.

A. Sampling and Analysis

The number of water samples taken and the sampling times were determined by the time scales of the physical processes to be investigated, and by the amount of available equipment. The ten experiments conducted can be divided into three groups. The first two experiments were preliminary tests to check equipment and procedures. For these tests, one water sample was taken from each of the three tank locations 120, 240, and 480 minutes after the oil was added. When visible changes in the oil slick were observed to take place within the first hour after the oil was added, a new sampling scheme was devised. In the next three experiments water samples were taken 10, 20, 40, 80, 160, 320, 480 and approximately 1440 minutes after the oil was added. The final sampling scheme, used in the last five experiments, was devised to document changes in oil dispersion with weathering and to obtain some estimate of the data scatter. At each sampling time, three 0.5 liter samples were taken from each of the three tank locations shown in Figure 3.34 for a total of nine samples per time. The sample times were 10, (only three samples were taken), 20, 160, 480, and approximately 1440 minutes after the oil was added. In all the experiments, three water samples to be used as background measurements were obtained before any oil was added to the tank. These samples were taken from the same three tank locations after the wave generator had run for one hour. In addition, samples were obtained one half hour after the wave generator was shut down.

B. Extraction Procedure

All the water samples obtained in these tests were analysed using a well known but tedious chemical extraction procedure. Briefly, the procedure involves washing the oil-water mixture a number of times with a solvent that dissolves the oil but is insoluble in water. In this case, CCl_4 was used. The oil concentration in the solvent was then determined by measuring the light absorbance at the fundamental resonant frequency of the carbon-hydrogen bond ($k-2930 \text{ cm}^{-1}$) on an infrared spectrophotometer. The absorbance is a linear function of the concentration of hydrocarbons present in the solvent. Thus the total amount of extractable hydrocarbons are measured. The concentration of hydrocarbons in the water sample due solely to the oil can be determined by subtracting out the background hydrocarbon concentration measure in the samples without oil. This entire analysis procedure has several disadvantages: it is expensive, time consuming, and extremely sensitive to contaminants. Unfortunately, there appears to be no better alternative.

Before any experiments were performed, the extraction procedure was extensively tested to document its efficiency and accuracy. It was found that violent agitation of the oil-water-solvent mixture increased the efficiency of the procedure dramatically. Calibration curves of absorbance verses concentration were created by mixing known quantities of Kuwait crude oil with CCl_4 and measuring the absorbance. A complete

discussion of the extraction procedure tests can be found in section 12.5.

The complete water sample analysis procedure that was used for all the oil dispersion experiments was as follows:

- i) All glassware was cleaned with laboratory cleaner (Alconox). Separatory funnels and dram bottles were rinsed with CCl_4 immediately before use.
- ii) Water samples were obtained by draining 0.5 liters of the tank water directly into 0.5 liter capacity separatory funnels fitted with teflon stopcocks and valves. A 30 ml aliquot of CCl_4 was then added immediately. The funnel was then shaken lightly and set aside for later extraction.
- iii) The oil was extracted by violently shaking the oil-water- CCl_4 mixture in the separatory funnel on a modified paint shaker for 20 seconds. The mixture was allowed to settle and separate for 15 minutes. The oil laden solvent was then slowly drained off into a dram bottle.
- iv) An additional 30 ml of CCl_4 was then added to the water remaining in the separatory funnel and step iii was repeated. The dram bottle was then tightly capped and stored in a dark place until the IR analysis was performed.
- v) The oil concentration was measured using a Perkin-Elmer Model no. 457 grating infrared spectrophotometer with 5 cm pathlength quartz cuvettes. The relative light transmittance z between k 3200 cm^{-1} and k 2930 cm^{-1} was determined by zeroing the machine at k 3200 cm^{-1} and letting it scan down to k 2800 cm^{-1} . The absorbance was then computed from a $\log_{10} (100/z)$, and the organic concentration in the CCl_4 was read off the calibration curve. Water sample organic concentration was then computed using the following equation:

$$[\text{Total Organic Concentration In Water (mg/l)}] = [\text{CCl}_4 \text{ Analyzed (ml)}] \times$$

$$\text{Total Organic Concentration In The CCl}_4 \text{ (mg/l)} \times \left[\frac{1 \text{ l}}{1000 \text{ ml}} \right] \times$$

$$\left[\frac{1}{\text{Water Sample Size (l)}} \right]$$

The estimated oil in water concentrations were established by subtracting out the background organic concentrations determined from the first three tank samples.

As a result of the preliminary experiments to test the extraction procedure, the overall extraction efficiency i.e., the percentage of the organic material extracted out of the water sample during each aliquot, was found to be about 90 percent. Because this is a relatively high value, in the interest of economy the second aliquot was not taken for some of the experiments. Consequently, all the concentration data

presented in Table 3.2 are computed from the results of one aliquot.

3.3.4. Oil Dispersion Experiment Test Procedure

The following standard experimental test procedure was used in the ten oil dispersion experiments:

- i) The tank and wave generating apparatus were cleaned thoroughly by scrubbing with a wire brush and solvent (National Chemsearch ND 150) and then rinsed completely.
- ii) The tank was filled to a depth of 71 cm (3470 liters) with either fresh or filtered salt water.
- iii) The wave generating hoop was installed and adjusted so that at the top of its stroke 1/4 of the hoop diameter was submerged. The hoop was adjusted to be parallel to the water surface. The desired generator speed, either 1.33 or 2.13 cycles per second was selected. The generator amplitude for all the experiments was fixed at 7.6 cm.
- iv) The wave generator was run for one hour at the desired speed. At the end of the hour, background water samples were taken from the three sampling locations shown in Figure 3.34. In addition, one liter surface samples to be used for water property measurements were also taken at this time.
- v) An 8 mm movie camera (Sankyo Super 8) was installed over the tank and adjusted to shoot either one frame every five seconds or every ten seconds. The camera was activated one minute before oil was added to the tank.
- vi) Standard Kuwait crude oil was added to the tank (60 or 120 ml.) by pouring down a glass plate to inhibit any initial dispersion.
- vii) Three 1/2 liter water samples were taken at the locations and times described in the sample analysis procedure. Samples were immediately preserved with the first aliquot of CCl_4 . 35 mm photographs were taken of the water surface and the water column directly after the sampling. Water temperature, air temperature, and any observations were also recorded.
- viii) The samples were processed as outlined in the sample analysis procedure.
- ix) The first three tests operated for a duration of eight hours while the last seven tests lasted for 24 hours. Additional water samples were taken 1/2 hour after the wave generator was shut down.

Table 3.2 Concentration Data, First Aliquot Only (Cont'd)

TIME	EXPERIMENT NO.									
(MIN.)	1	2	3	4	5	6	7	8	9	10
320										
1			6.53	26.26	4.14					
2			7.92	11.10	2.54					
3			4.99	14.84	3.71					
480										
1a	.85	.60	7.77	18.77	3.93	19.5	33.3	* 8.73	3.32	8.17
1b						10.0	16.5	4.97	3.95	6.91
1c						8.58	25.0	37.8	2.82	10.39
2a	.84	.40	4.28	10.63	3.32	11.7	9.88	2.57	2.99	8.02
2b						6.93	5.62	2.27	2.67	7.71
2c						8.29	4.64	5.46	3.16	6.83
3a	.54	.58	4.97	5.21	3.85	11.4	4.34	.77	2.92	15.22
3b						7.42		2.74	1.80	6.03
3c						5.58	3.82	1.92	.86	7.64
1440*										
TIMES				1340	1440	1430	1495	1495	1595	1760
1a			* 2.72		3.03	* 20.7	* 9.47	** 19.7	* 31.41	* 8.38
1b						17.6	3.26	2.89	31.13	7.15
1c						15.1	1.58	3.42	83.31	
2a				24.75	2.43	19.2	5.05	3.29	88.91	7.77
2b						19.4	1.10	1.20	10.38	8.86
2c						12.7	2.21	.53	8.79	7.78
3a				1.53	2.73	37.4	4.56	.92	15.64	13.08
3b						10.2	1.44	.44	4.32	12.12
3c						11.2	2.38	2.84	4.29	5.89
Wave Generator Shut Down Time	490	490	490	1360	1450	1440	1510	1500	1605	1780

*NOTE: 1440 minutes is the nominal time for the last water samples.
The actual sampling times are listed in each column.

3.4. CHARACTERISTICS OF EXPERIMENT

3.4.1. WAVE MEASUREMENTS

Sample water surface elevation records for four of the wave staff locations shown in Figures 3.3 and 3.4 are presented in Figures 3.5 through 3.8. The data for these plots was extracted from much longer samples used for a spectrum analysis. Note the difference in amplitude scales from figure to figure.

A. Observations

The wave patterns produced by the wave generator operating at 1.33 cycles per second are shown in Figures 3.9 through 3.13. These figures are all photographs taken of experiment 6. Figure 3.9 shows the regular concentric wavefronts spaced approximately 9 inches apart. Here they continue all the way to the tank center and concentrate the oil in a small area. By contrast, Figure 3.10 shows a more random pattern of waves with a much larger region of oil submergence. Generally, the oil was dispersed by either breaking or collapsing waves within a 36 inch diameter region at the center of the tank, and the random pattern of Figure 3.10 was more prevalent. However, the most intense breaking and the highest waves usually occurred at the center.

The waves created at the 1.33 cycle per second generator frequency ranged in height from one to six inches at the tank center. They were generally steeper than waves normally seen in the ocean. Figures 3.11 through 3.13 show some of the different wave shapes produced. Most waves resembled plunging breakers often seen at beaches (Fig. 3.11). Other waves were shaped like small pyramids and would collapse straight back on themselves (Fig. 3.12). In the most extreme cases, the disturbance resembled small jets of water that would shoot straight up about six inches and then fall straight back into the water column (Fig. 3.13). The frequency of occurrence of any of these wave shapes appeared to depend on the radial symmetry of the wavefronts created, with the most symmetric wavefronts producing the most extreme and localized disturbances. Although it was possible to affect the location of the most intense wave action by tilting the generating hoop, it was not possible to create a given type of wave simply by changing adjustments. The wave pattern existing at any given time depended on the interaction between the generated waves, the waves reflected off the tank walls, and the waves that had previously interfered and collapsed.

The actual water surface area covered by each individual breaking wave ranged up to 1 inch by 3 inches. The median area can be estimated by observation to be about 1 by 2 inches. While the waves in the tank clearly collapse as do breaking waves in the ocean, much less air is entrained by the water. Consequently, the waves do not have the characteristic appearance of "whitecaps". Each collapsing wave injected a plume of water into the water column which could be visualized by following the motion of oil droplets or entrained air bubbles. The observed plume depth was directly related to the height of the collapsing surface

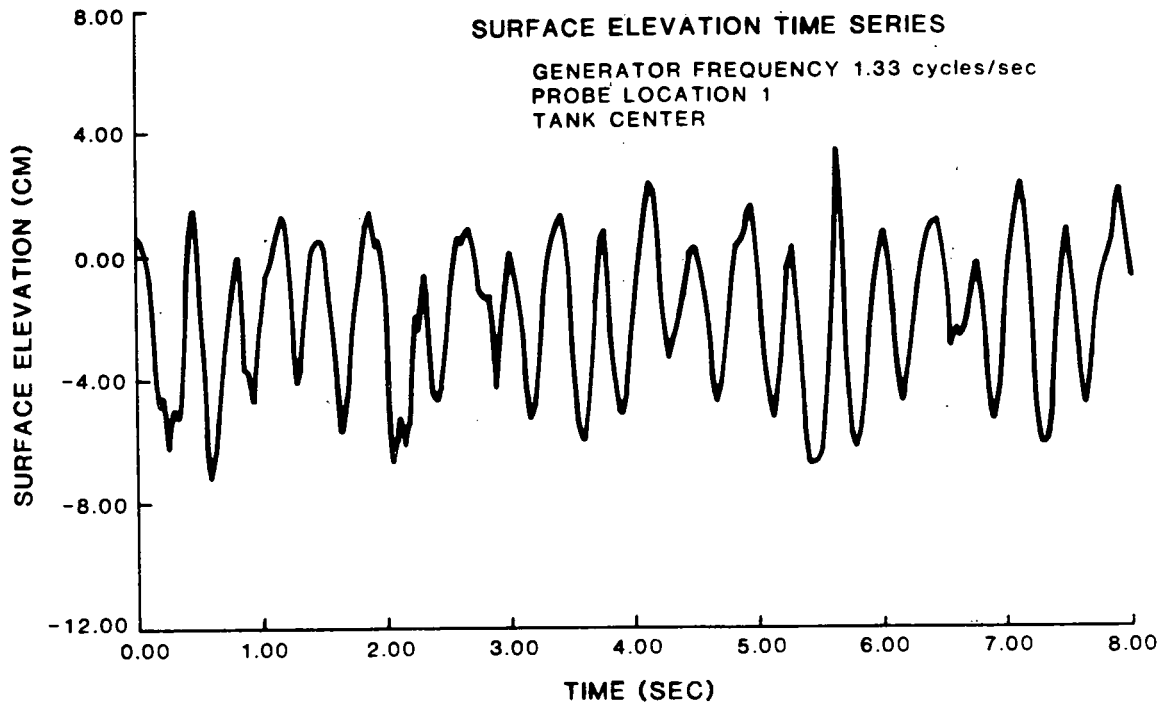


Figure 3.5. Surface Elevation Time Series Probe Location 1

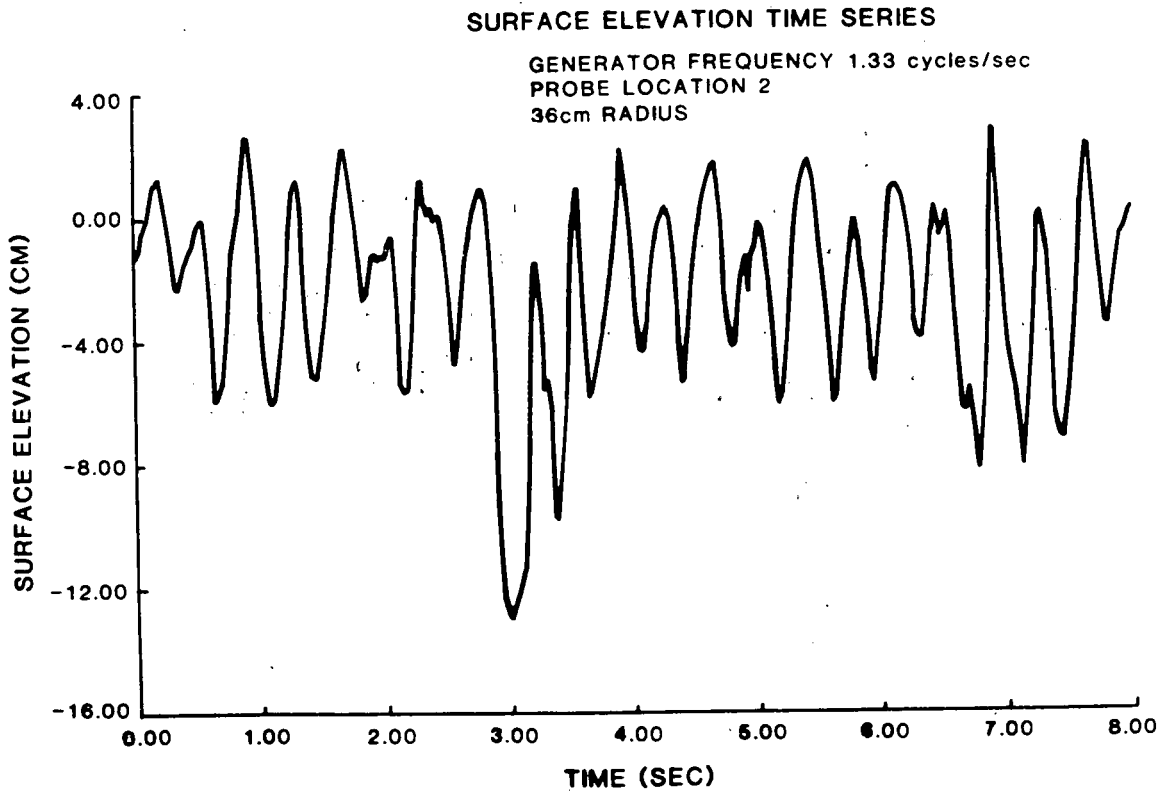


Figure 3.6. Surface Elevation Time Series Probe Location 2

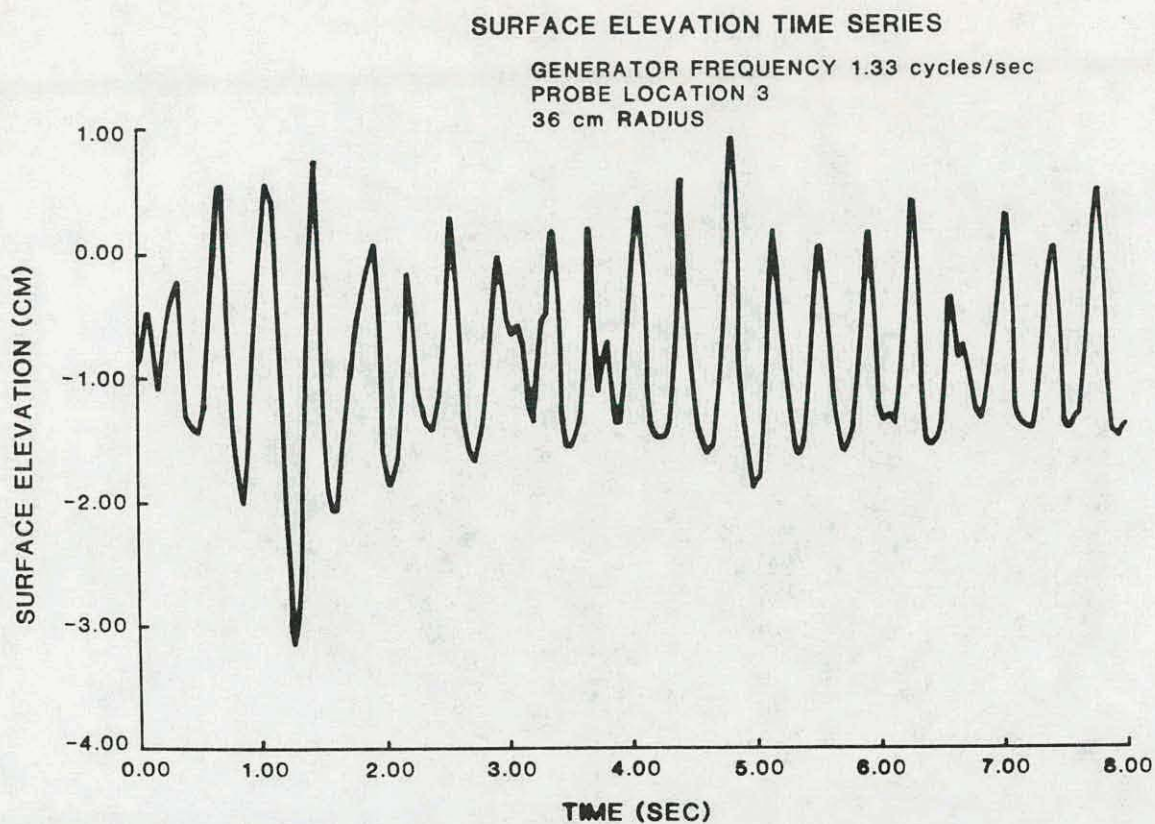


Figure 3.7. Surface Elevation Time Series Probe Location 4

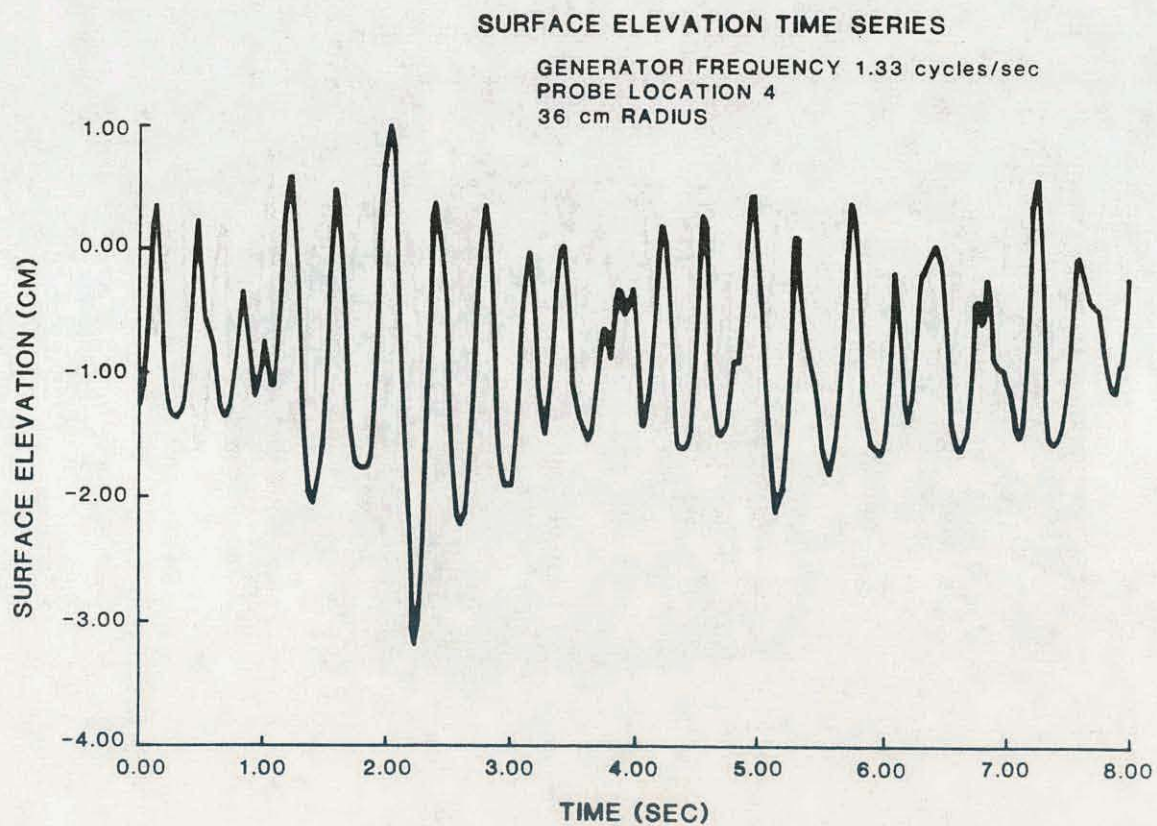


Figure 3.8. Surface Elevation Time Series Probe Location 4

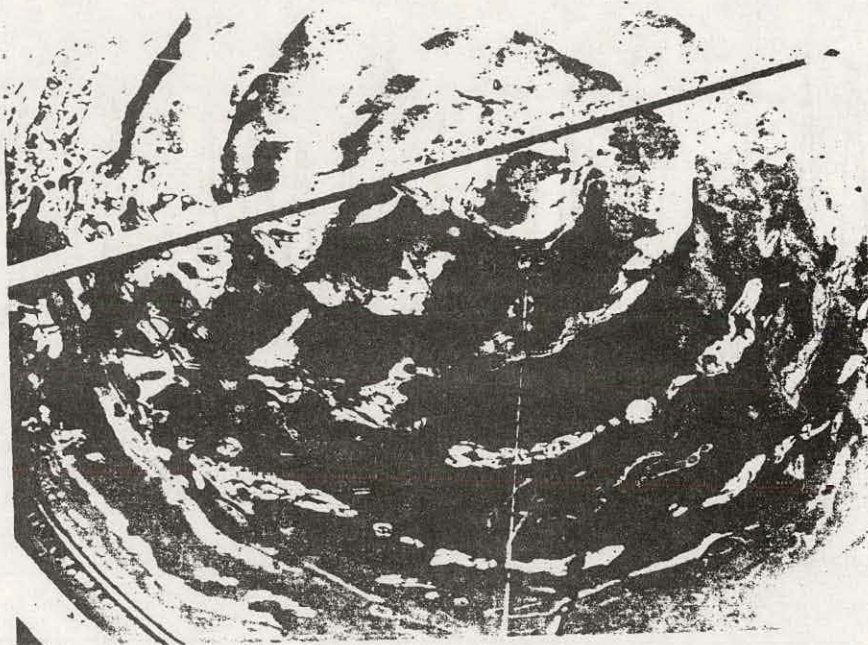


Figure 3.9. Wave Fronts 1.33 CPS

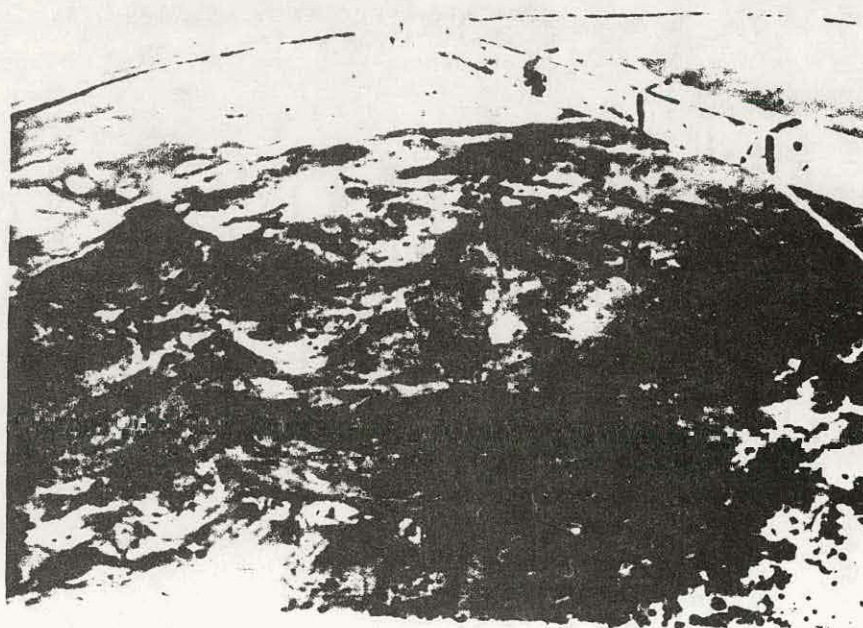


Figure 3.10. Random Waves at Center

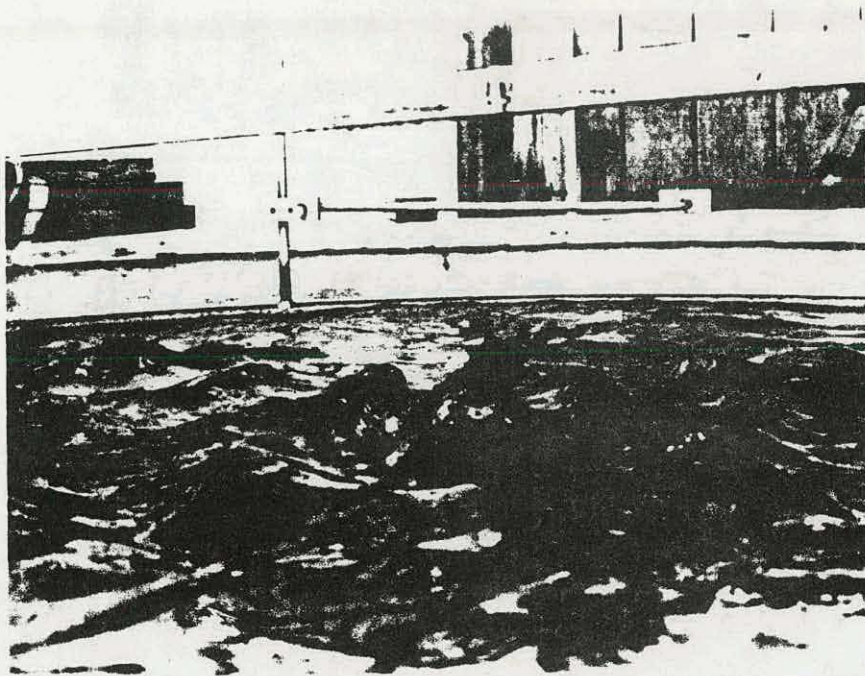


Figure 3.11. Wave Shapes

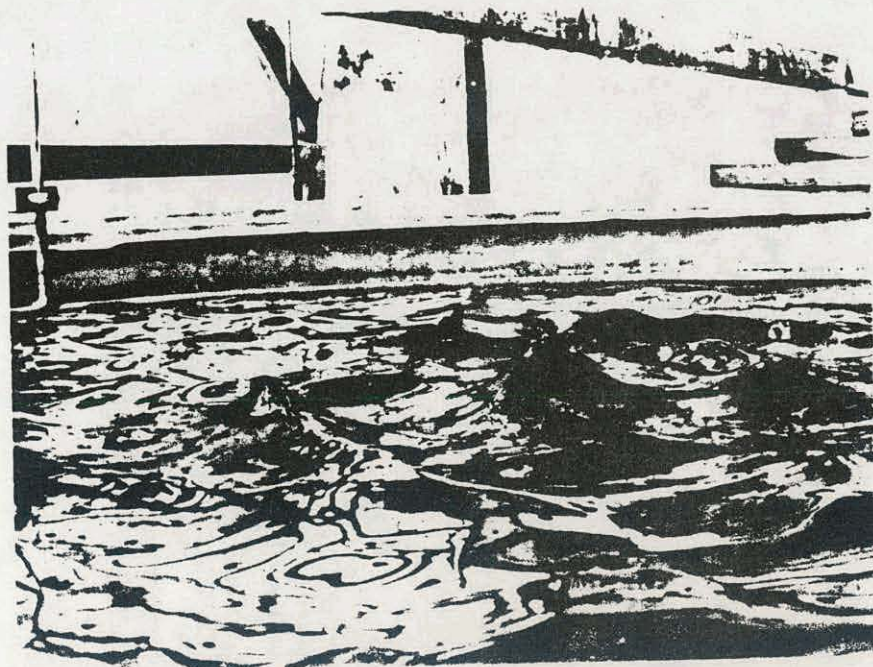


Figure 3.12. Wave Shapes

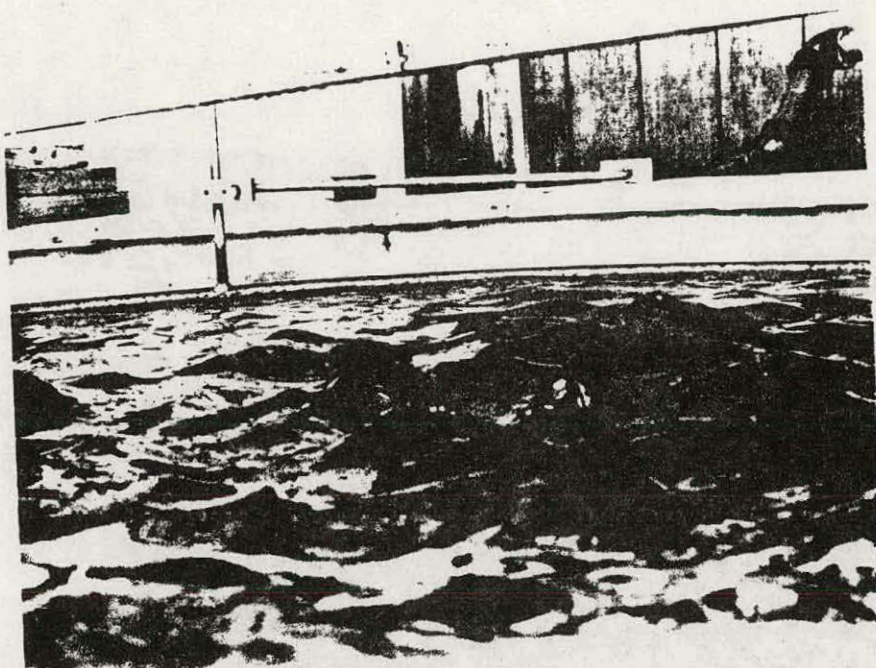


Figure 3.13. Wave Shapes

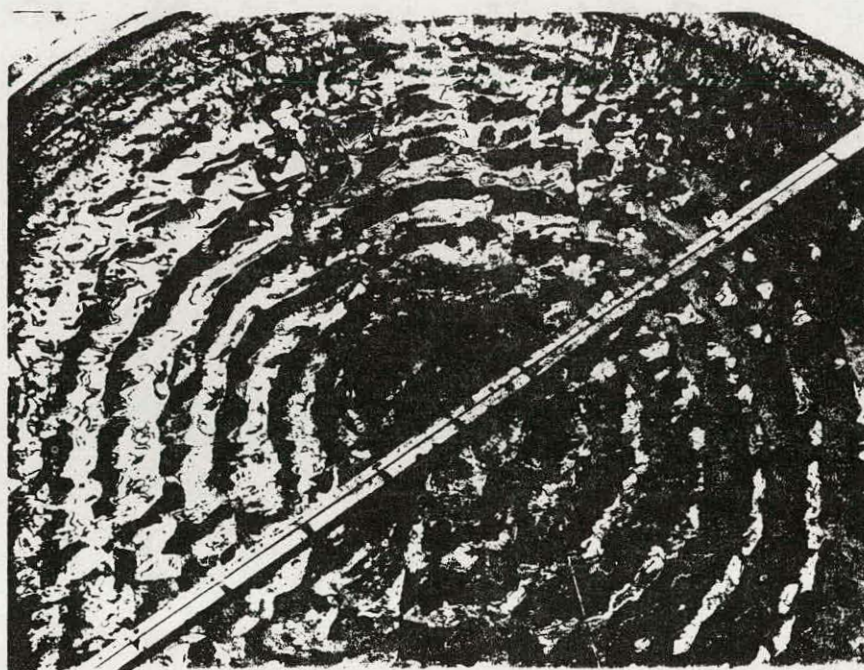


Figure 3.14. Wave Pattern 2.13 CPS



Figure 3.15. Wave Pattern 2.14 CPS

wave, and in all cases the depth appeared to be roughly equal to the wave height.

Waves created at the faster (2.13 cycle per second) wave generator frequency are more closely spaced, smaller, and caused less intense individual disturbances in the tank. Figure 3.14 through 3.15, taken of tests 5 and 7, show the wave characteristics. From Figure 3.14 the crest to crest distance can be estimated at about 4 inches. It can also be seen that the oil is contained in a much smaller region (approximately 18 inches in diameter). The smaller waves did not display the variety of shapes evident at the lower generator frequency. Most of the waves near the tank center were pyramid shaped and tended to collapse back upon themselves. (See Fig. 3.15).

B. Results and Discussion

Applying fourier transforms to the recorded wave data results in the power spectral density plots shown in Figures 3.16 to 3.23. The transformations confirm that the dominant frequency of the waves produced by the generator operating at 1.33 cycles per second is 2.67 cycles per second, or twice the generator frequency. The waves produced by the 2.13 cycle per second generator frequency have important components at 2.1 and 4.2 cycles per second.

The total ENERGY, potential and kinetic, per unit area of the water surface contained in a simple harmonic progressive wave train equals (Ref. 3.2):

$$1/2 \rho g a^2 \text{ or } 1/8 \rho g H^2$$

where

$$\begin{aligned} \rho &= \text{water density} \\ g &= \text{gravitational acceleration} \\ \text{and } H &= 2a = \text{wave height.} \end{aligned}$$

The ordinate in the graphs of the wave spectral distribution is in units of the square of the fourier coefficients or the square of the amplitudes of the frequency components. Thus the ordinates are in units of wave energy. The root mean square wave height may be obtained by integrating under the spectral peaks and taking the square root:

$$H_{\text{RMS}} = 2 \sqrt{\int_0^{\infty} [a(f)]^2 df}$$

and

$$H_{\text{peak}} = \sqrt{2 H_{\text{RMS}}}$$

a numerical integration of the fourier transformed wave data was performed using a trapazoidal approximation. The results are presented below:

POWER SPECTRUM

GEN. FREQ. = 1.33 CYCLES/SECOND PROBE LOCATION 1. (FIG. 3.3)
 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz 100 ENSEMBLES AVERAGED

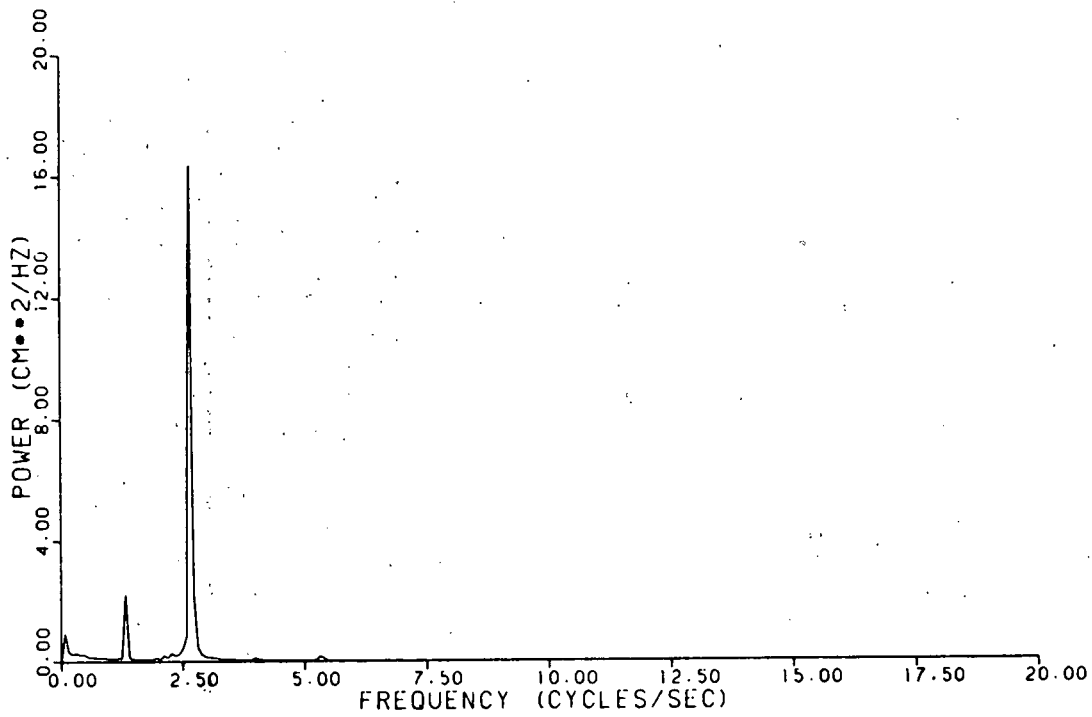


Figure 3.16. Power Spectrum Probe Location 1 512 Pt. Transform

POWER SPECTRUM

GEN. FREQ. = 1.33 CYCLES/SECOND PROBE LOCATION 2.
 36 CM RADIUS 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz
 100 ENSEMBLES

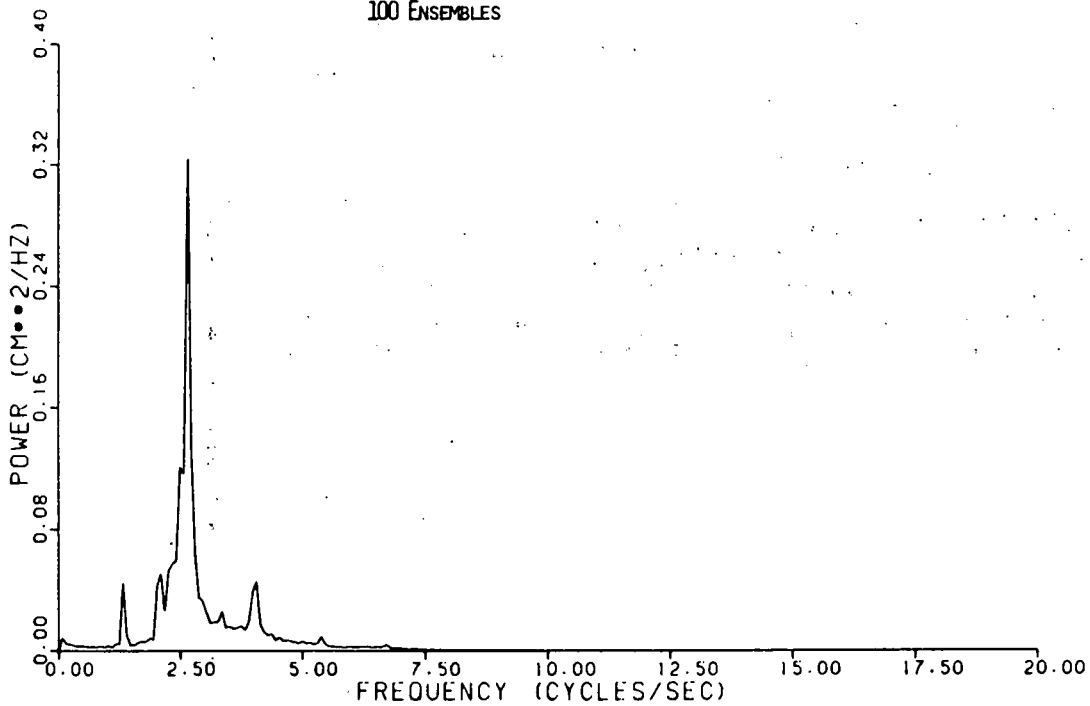


Figure 3.17. Power Spectrum Probe Location 2 36 cm Radius

POWER SPECTRUM

GEN. FREQ. = 1.33 CYCLES/SECOND PROBE LOCATION 3.
 36 CM RADIUS 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz
 100 ENSEMBLES AVERAGED

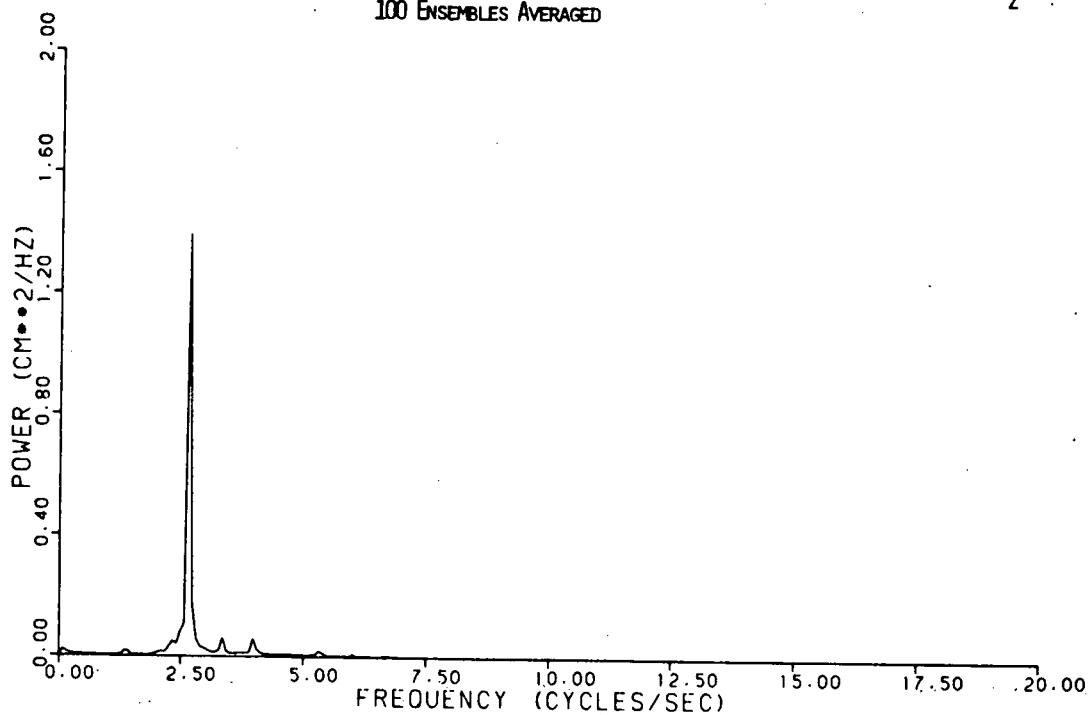


Figure 3.18. Power Spectrum Probe Location 3 36 cm Radius

POWER SPECTRUM

GEN. FREQ. = 1.33 CYCLES/SECOND PROBE LOCATION 4.
 36 CM RADIUS 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz
 100 ENSEMBLES AVERAGED 2ND DATA SET

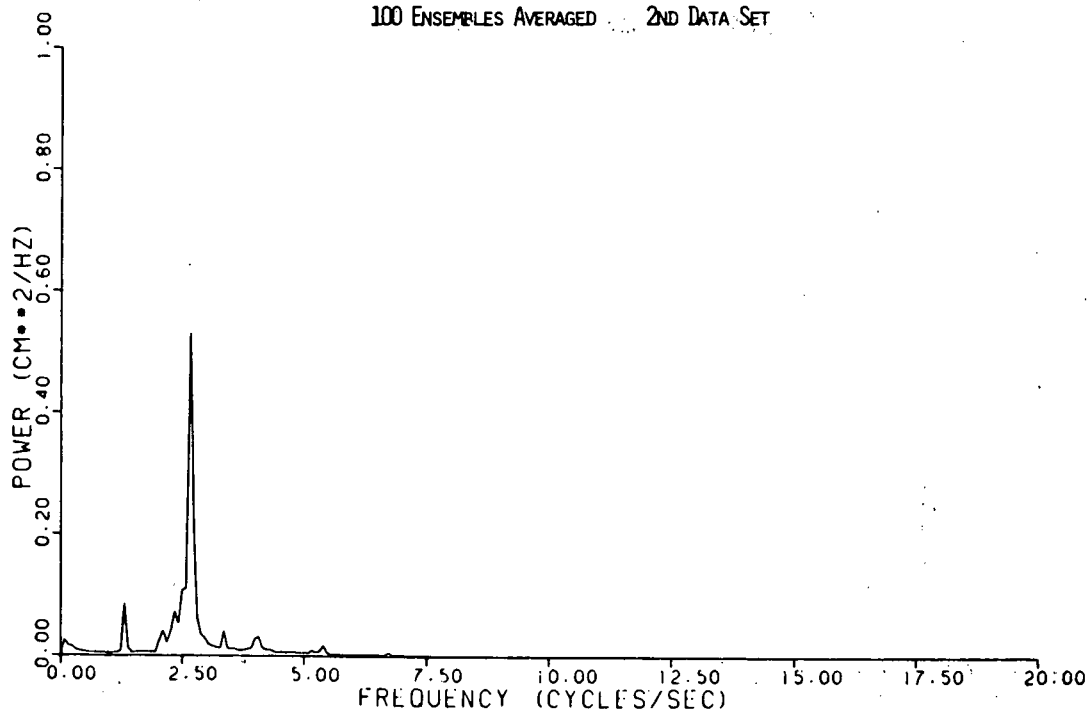


Figure 3.19. Power Spectrum Probe Location 4 36 cm Radius

POWER SPECTRUM

GEN. FREQ. = 2.13 CYCLES/SECOND PROBE LOCATION 1, TANK CENTER (FIG. 3.4)
 512 PT. TRANSFORM FREQ. RESOLUTION = .08 H_z 75 ENSEMBLES AVERAGED

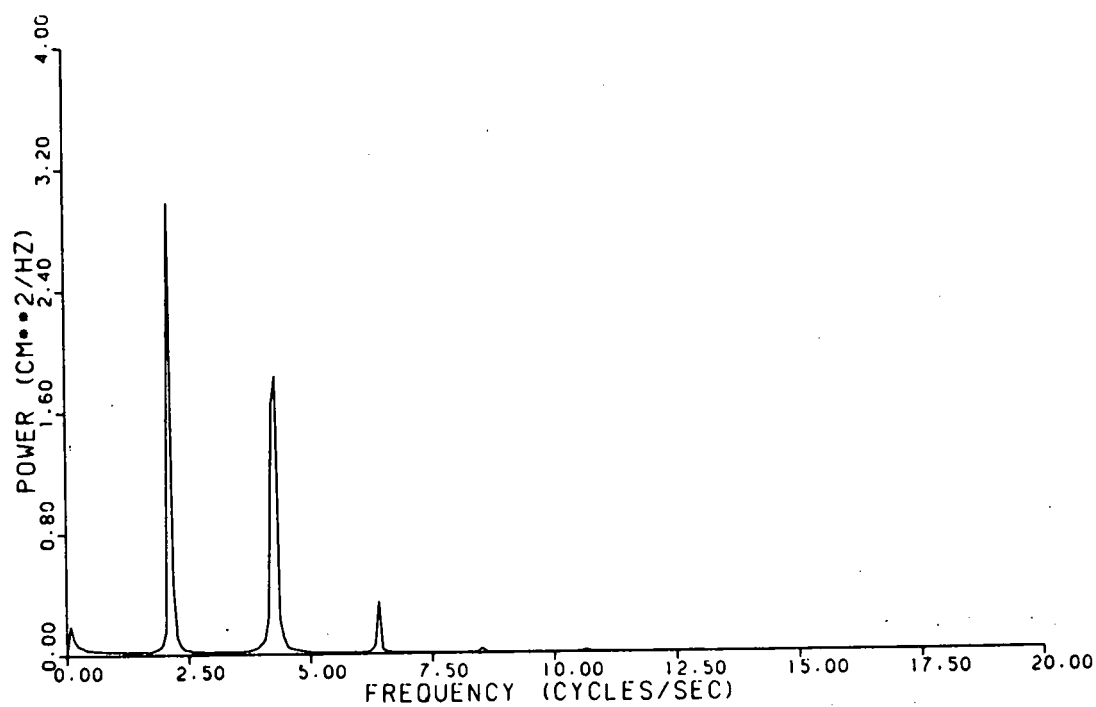


Figure 3.20. Power Spectrum Probe Location 1 512 Pt. Transform

POWER SPECTRUM

GEN. FREQ. = 2.13 CYCLES/SECOND PROBE LOCATION 2,
 25 CM RADIUS 512 PT. TRANSFORM FREQ. RESOLUTION = .08 H_z
 75 ENSEMBLES AVERAGED

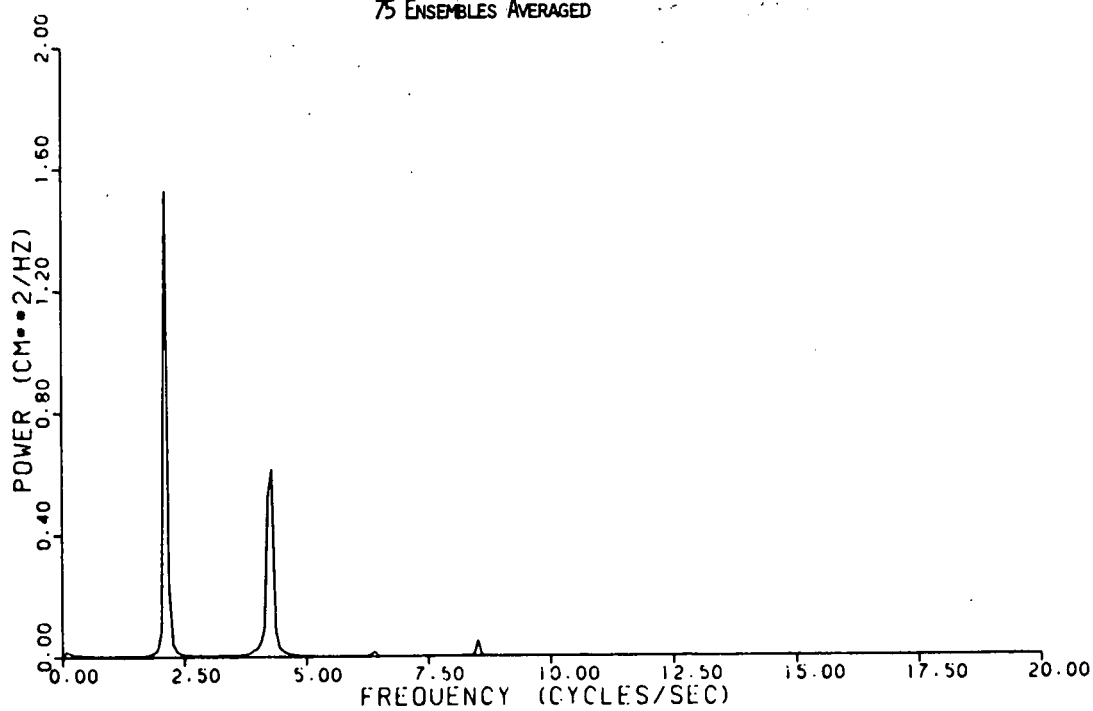


Figure 3.21. Power Spectrum Probe Location 2 25 cm Radius

POWER SPECTRUM

GEN. FREQ. = 2.13 CYCLES/SECOND PROBE LOCATION 3.
 13 CM RADIUS 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz
 75 ENSEMBLES AVERAGED

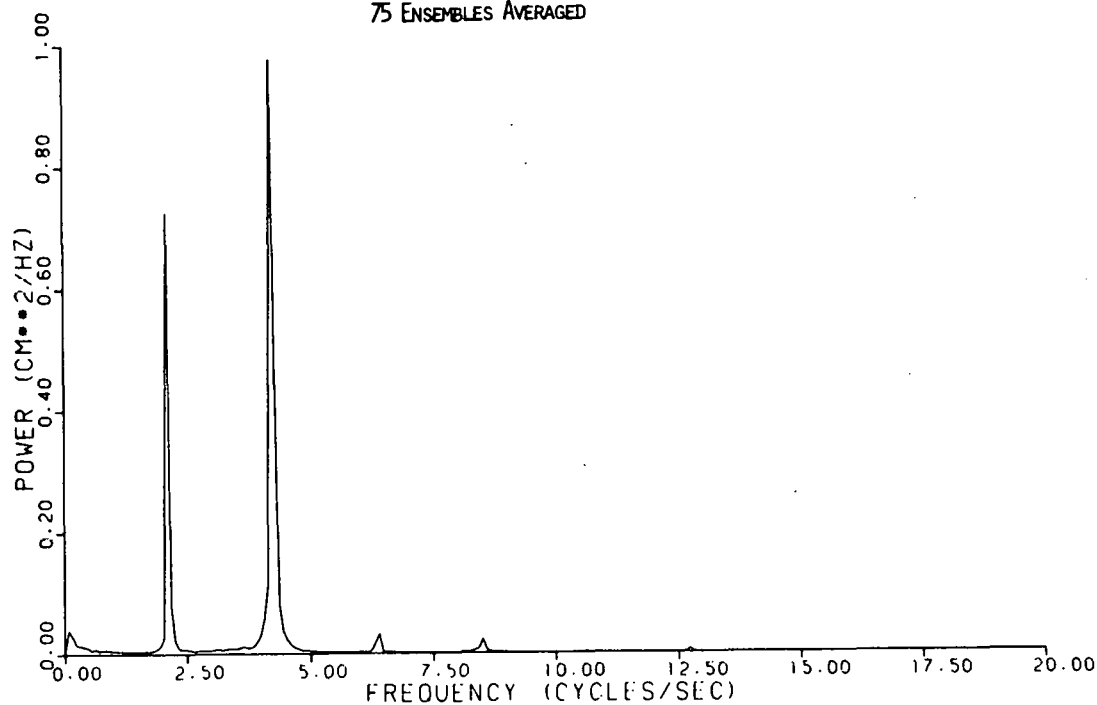


Figure 3.22. Power Spectrum Probe Location 3 13 cm Radius 512 Pt. Transform

POWER SPECTRUM

GEN. FREQ. = 2.13 CYCLES/SECOND PROBE LOCATION 4, 13 CM RADIUS
 512 PT. TRANSFORM FREQ. RESOLUTION = .08 Hz 75 ENSEMBLES AVERAGED

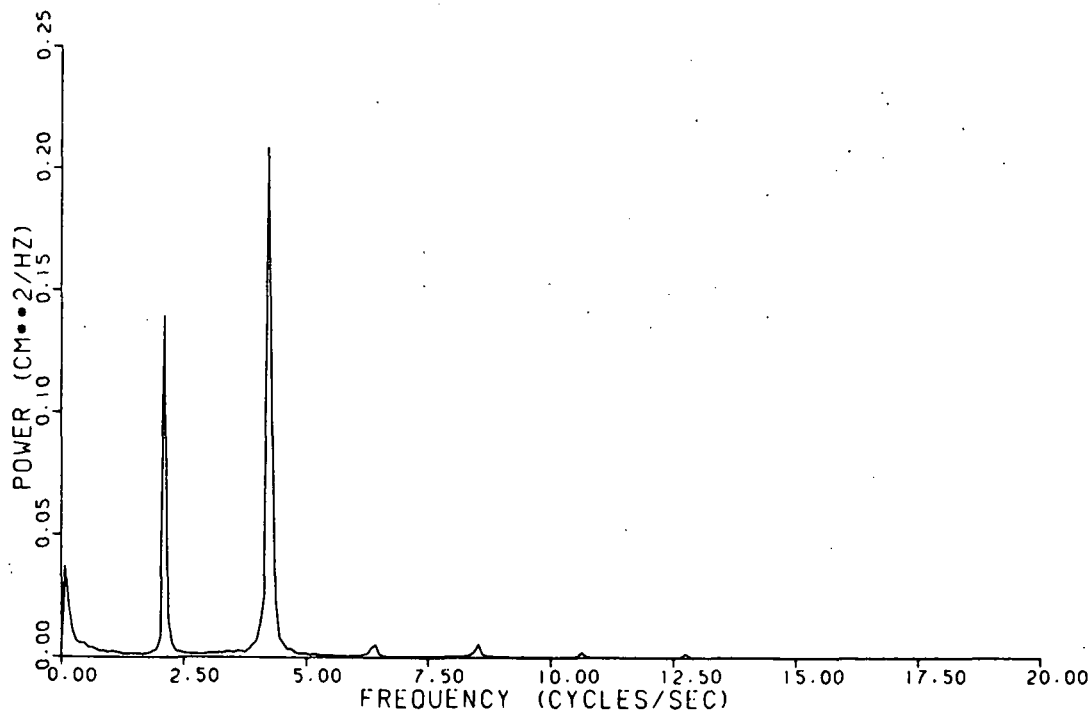


Figure 3.23. Power Spectrum Probe Location 4 13 cm Radius 512 Pt. Transform

Expt. 1 Wave Generator Frequency = 1.33 cycle/second

1. Measurement Location: (see Fig. 3.3)	1	2	3	4
2. Wave Frequency: (cycles/second)	2.67	2.67	2.67	2.67
3. Peak to Peak Wave Height: (cm)	6.2	1.8	1.4	1.6

Expt. 2 Wave Generator Frequency = 2.13 cycles/second

Measurements Location: (see Figure 3.4)	1	2	3	4
Wave Frequency (cycles/second)	2.1	2.1	2.1	2.1
Peak to Peak Wave Height: (cm)	2.4	1.6	1.2	0.4
Wave Frequency: (cycles/second)	4.2	4.2	4.2	4.2
Peak to Peak Wave Height: (cm)	2.4	1.4	1.6	0.8

The results show that except for Location 4 of the second experiment, the waves are approximately the same average height at equal tank radii, and that the wave height grows as the waves approach the center, which is expected from energy conservation principles. As the wave fronts travel toward the center of the tank, the energy per unit area must remain the same (not counting frictional losses). This is accomplished by an increase in wave height until a limiting value is reached at which point the wave collapses. Examination of the wave data from location 4 of the second experiment show that after about ten minutes, the recorded wave amplitudes are significantly lower. It is believed that the wave probe was fouled by debris in the tank making the data from this probe suspect.

A theory for water waves of finite heights was developed by Stokes in the nineteenth century. The theory solves the wave equation with the wave parameters input in the form of a truncated infinite series. Results are also in series form. A discussion of the second and third order results can be found in Ref. (3.2) and (3.3). The second order theory gives the following equation for the wavelength and celerity.

$$L = \frac{gT^2}{2\pi} \tanh \left(\frac{2\pi h}{L} \right)$$

$$C = \frac{gT}{2\pi} \tanh \left(\frac{2\pi H}{L} \right)$$

If the quantity in parentheses is large (> 3), the value of the hyperbolic tangent is approximately 1, and the equation may be simplified to:

$$L = \frac{gT^2}{2\pi}$$

$$C = \frac{gT}{2\pi}$$

Generally, this simplification is valid if $h/L > 4$. Since the observed wavelengths of the waves in the tank are about 4 inches (10.2 cm) and 9 inches (22.9) (see the photographs in Figures 3.14 and 3.9) for the 2.13 cycle/second and 1.33 cycle/second wave frequencies respectively the above criteria are satisfied. The results from substituting the appropriate wave periods identified from the spectral plots into these simplified equations are presented in the following table:

Table 3.3.

Wave Frequency	Wave Period (sec)	Wavelength (cm)	Wave Celerity (cm/sec)
2.67	.375	21.9	58.5
2.1	.476	35.3	74.2
4.2	.238	8.8	37.1

It can be seen that the wavelength computed for the 2.67 and 4.2 cycle per second wave frequencies are in reasonable agreement with observed lengths. The Stoke's wave theory also predicts that the steepest water waves will have a crest angle of 120 degrees, or alternatively that the wave height divided by the length will be less than 0.142: i.e.,

$$H/L \leq .142 \approx 1/7$$

for stable waves. Steeper waves will collapse and break.

Using the data computed above, height to length ratios have been computed for the 2.67 and 4.2 cycle per second water waves:

Wave frequency = 2.67 cycle per second

Probe location (see Fig. 3.3 and 3.4)

	1	2	3	4
H/L	.28	.08	.06	.07

Wave Frequency = 4.2 cycles per second

H/L	.27	.16	.18	.09
-----	-----	-----	-----	-----

The results show that for both the 2.67 and 4.2 cycle per second surface waves, the breaking criteria is exceeded at the center position.

3.4.2. CURRENT MEASUREMENTS

A. Observations

The directions and relative magnitudes of the currents and eddies in the tank were found by observing the motions of dye plumes and neutrally buoyant particles from numerous tank locations. A sketch of a tank section showing an estimated current profile derived from these observations is given in Figure 3.24. It can be seen that the influx of water toward the tank center occurs in a shallow path with relatively high water velocities. This path is 5-8 cm deep at the 1.33 cycles per second generator frequency and 4-5 cm deep at the 2.1 cycles per second frequency. The return flow travels out and down from the center of the tank in the shape of a shallow cone. The interface between these two flows is not well defined. Just beneath the surface flow is a layer of slow moving water with no preferred direction. Also, at the corner between the tank wall and floor, and in the small space behind the wave generator, back eddies were observed.

The currents and eddies near the center of the tank depended on the surface wave action, and hence varied significantly at any given location over time. Individual plunging waves might superimpose a rapidly moving plume of water on the general downward flow at the center. Or, the rapid inflow of water could be interrupted by a wave tumbling against the current. A roughly circular region at the center of the tank was defined by a ring of surface water with no average radial velocity. This ring was formed when the radial inflow induced by the water waves met water tumbling away from the center from collapsing or breaking waves. This ring forms a convenient boundary. Inside the ring is the region of intense breaking wave action and outside the ring waves are regular and the wave fronts are circular. When small pieces of paper were scattered over the entire surface of the tank and allowed to migrate toward the center, the maximum distance the paper would reside from the center of the tank would be the radius of this ring. Indeed, this was also the maximum radius of the experimental oil slicks. The approximate maximum radius of the center region was 55 cm at the slow generator frequencies and 40 cm at the fast frequency. However, the dimensions would expand and contract depending on the wave intensity in the tank.

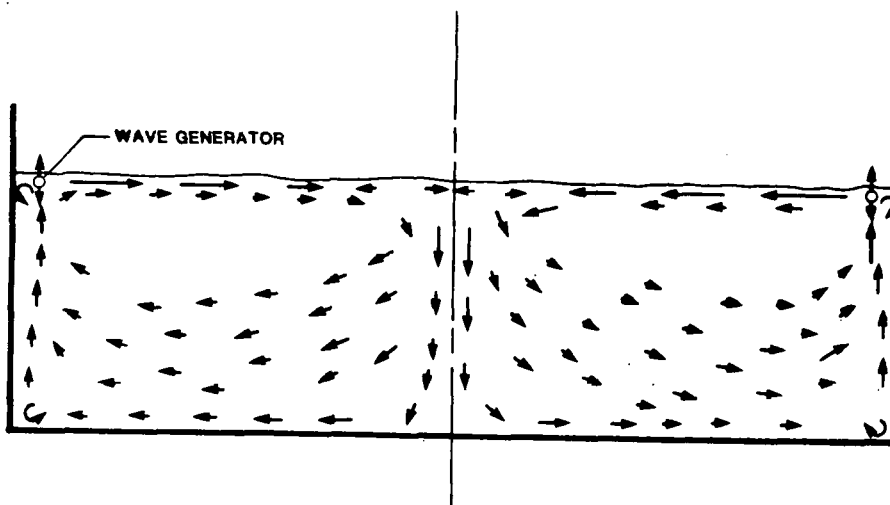


FIGURE 3.24
CURRENT PATTERN

The water at the center region of the tank would rotate as a whole with smaller eddies contained inside. The maximum rotational velocity was estimated to be .05 to .3 radius per second. However, the rotation was not steady or consistent. No preferred direction of rotation was observed, nor was any regular frequency of direction change apparent.

The average velocity of the water travelling the entire convective path from the tank center down and out to the edge, and back to the center again, was found by determining the time difference between successive dye concentration peaks resulting from a plume of dye injected into the flow and sampled at the tank wall. Data from four experiments with 30 ml of dye applied to the center of the tank are shown in Figures 3.25 to 3.31. Input conditions, generator frequencies and sampling locations are listed on the figures. The ordinate in all the figures has been normalized by the uniform tank concentration resulting from 30 ml of dye mixed with 3470 liters of tank water. Dye sampling locations are shown in Fig. 3.32. The dye was then added at the center and water samples for the first two experiments were taken from locations 1 and 3 shown in Figure 3.32. Samples for the third experiment were taken from locations 1 and 2 and samples for the last experiment were taken only from location 1. First the tank was filled with fresh water and the wave maker run for one hour. Additional measurements of the surface currents were performed by timing the motion of .5 cm square paper drifters migrating toward the center of the tank. The tracks over which the drifters were observed are shown in Figure 3.33. The data is listed in Table 3.4.

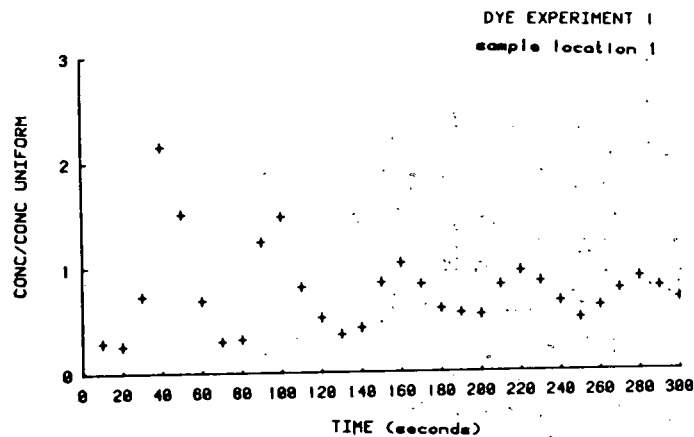


Figure 3.25. Dye Experiment 1 Sample Location 1

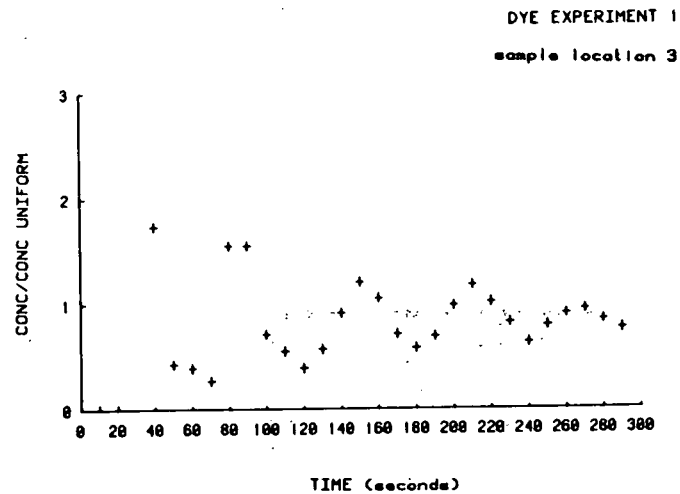


Figure 3.26. Dye Experiment 1 Sample Location 3

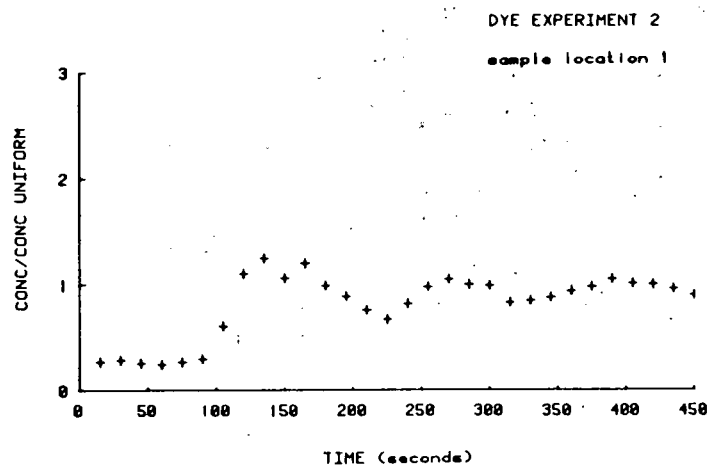


Figure 3.27. Dye Experiment 2 Sample Location 1

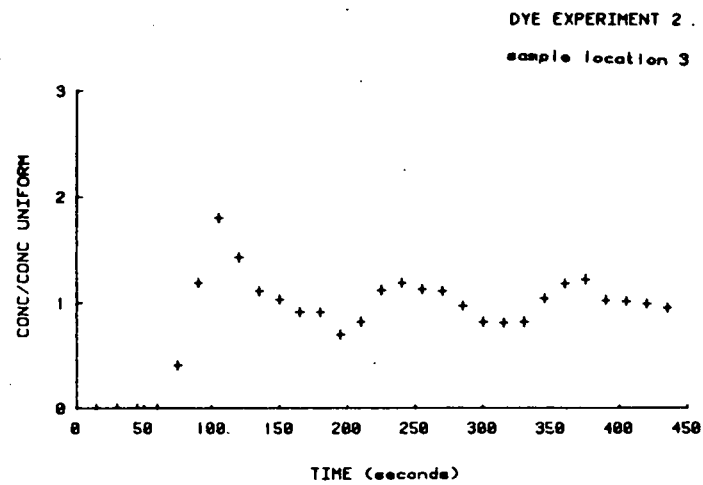


Figure 3.28. Dye Experiment 2 Sample Location 3

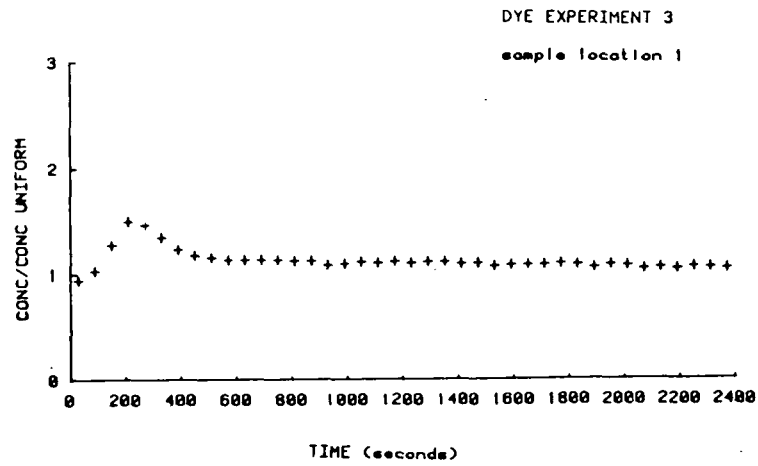


Figure 3.29. Dye Experiment 3 Sample Location 1

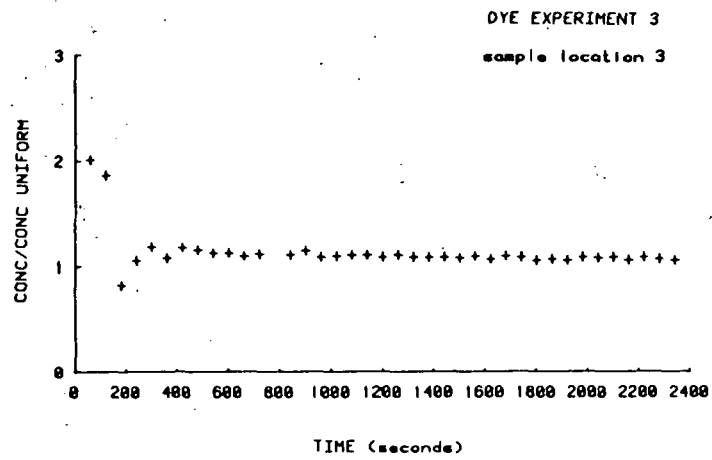


Figure 3.30. Dye Experiment 3 Sample Location 3

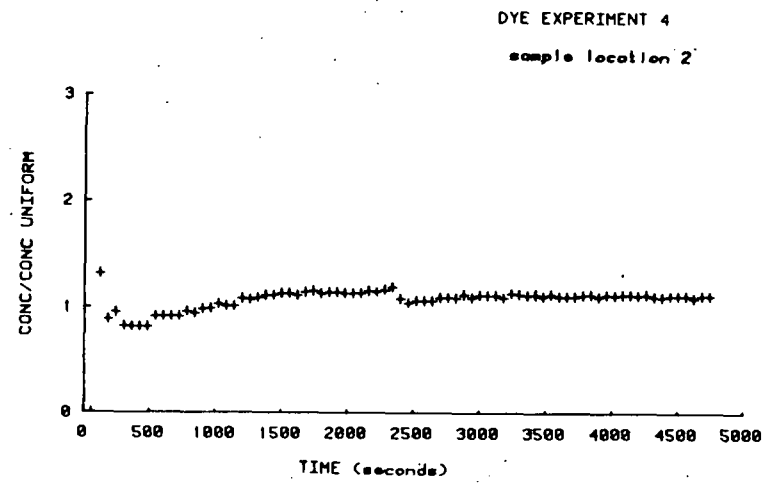


Figure 3.31. Dye Experiment 4 Sample Location 2

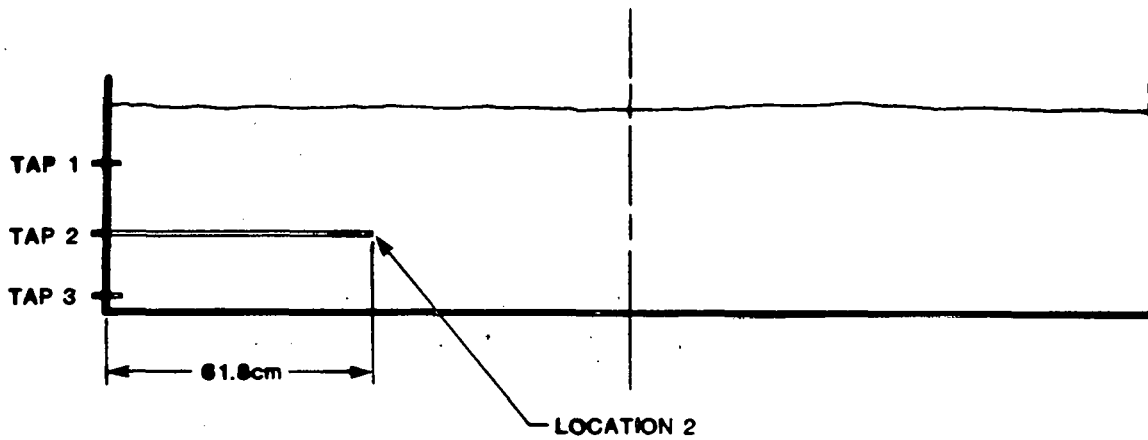
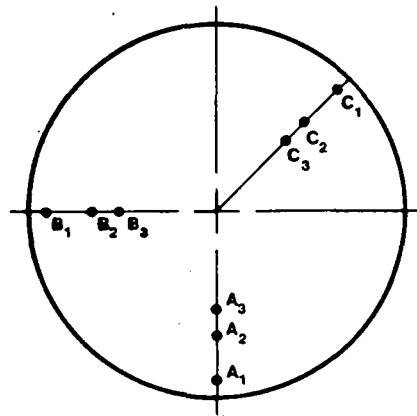


FIGURE 3.32
DYE SAMPLING LOCATIONS



RADI $A_1 = B_1 = C_1 = 112.4\text{cm}$
 $A_2 = B_2 = C_2 = 79.4\text{cm}$
 $A_3 = B_3 = C_3 = 64.1\text{cm}$

NOTE 1 :

All the radii measurements are referenced to the centerline of the wave generating hoop.

NOTE 2 :

$A_3 = 48.9\text{cm}$ for the 2.13 Hz tests.

FIGURE 3.33
PATHS OVER WHICH DRIFTERS WERE TIMED

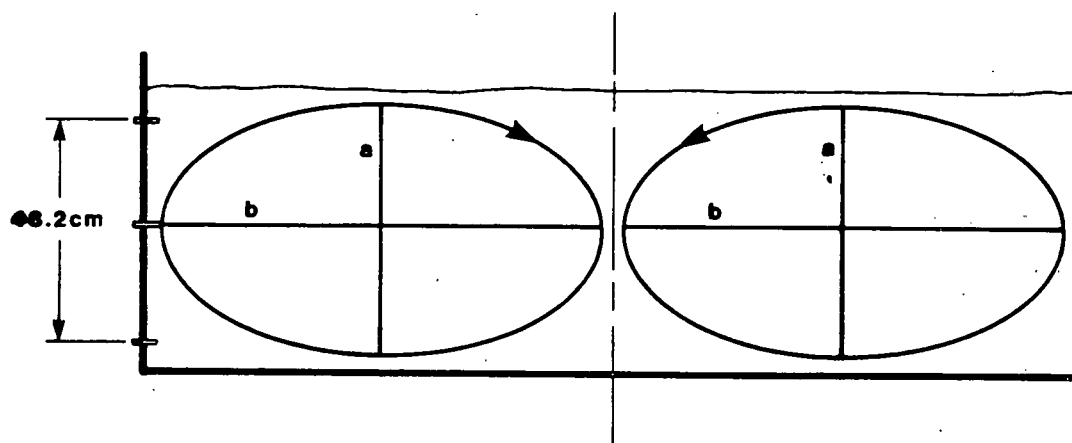
TABLE 3.4. TRAVEL TIMES FOR PAPER DRIFTERS (seconds)

Wave Generator Frequency:							
1.33 cycles/second				2.13 cycles/second			
Location: (see figure)							
A_1A_2	A_1A_3	B_1B_2	B_1B_3	C_1C_2	C_1C_3	A_1A_2	A_1A_3
3.1	9.5	3.5	6.0	4.2	7.8	2.5	6.0
4.8	10.5	3.2	4.5	2.9	7.4	2.9	8.1
4.0	7.1	3.8	5.5	4.6	6.9	2.5	8.1
4.7	6.6	3.6	5.5	3.5	6.6	2.2	6.9
3.6	12.9	3.6	5.0	3.3	6.1	2.4	6.9
4.8	13.0	3.6	6.6	5.0	7.4	2.8	8.5
3.3	9.6	3.5	6.5	4.1	8.2	2.5	7.3
3.2	6.1	4.2	5.0	2.4	6.2	2.5	7.3
4.0	12.9	3.0	4.9	2.9	5.1	2.6	7.4
4.6	8.5	3.4	8.2	3.3	7.0	2.5	8.8
4.1	9.6	2.4	7.2	3.9	6.9	3.0	7.0
4.0	7.2	3.1	4.6	3.5	6.4	2.8	5.7
4.7	8.4	3.6	5.4	4.4	6.8	2.4	7.1
4.3	8.8	3.8	6.4	3.4	8.4	2.7	8.9
3.9	6.5	2.9	5.0	2.7	6.1	2.7	5.7
4.1	8.4	2.6	7.3	3.6	8.2	3.0	7.1
4.9	10.5	3.3	5.6	3.3	6.8	2.6	7.5
3.2	9.8	3.1	6.6	2.9	6.7	2.1	7.5
4.0	7.5	2.6	4.7	4.6	5.8	2.4	5.9
5.4	7.4	4.4	5.4	3.7	8.4	2.9	7.3
4.3	10.4	3.2	6.4	3.8	6.2	2.3	7.3
4.3	6.0	3.3	6.8	3.7	6.0	2.7	7.2
4.0	10.9	3.5	5.0	3.9	6.2	2.5	6.1
4.2	6.3	3.0	5.9	4.0	6.9	2.6	7.4
4.5	5.9	3.6	4.6	3.6	7.3	2.5	7.5
3.1	9.8	3.3	4.4	2.7	6.6	2.0	7.8
4.0	9.4	2.9	4.5	3.4	5.8	2.7	6.5
5.3	7.8	3.0	5.8	2.8	7.1	2.8	5.9
4.5	7.2	2.9	5.1	3.2	8.8	2.3	7.4
4.3	11.5	3.3	4.8	3.4	6.8	2.7	6.0
			5.7				5.6
			6.0				

B. Results and Discussion

The dye concentration verses time graphs from the first two tests clearly show the series of dye concentration peaks resulting from the dye plumes in the recirculating flow crossing the sampling locations. The concentration peaks become lower and broader with each successive cycle as the dye diffuses forward and backward into the flow stream. The concentrations also tend toward the uniform value representing complete mixing in the tank.

If each plotted concentration peak is assumed to represent the center of the dye plume, and the water is assumed to follow the elliptical path shown in the figure below, the average circulation velocity can be determined by dividing the path length by the mean time difference between concentration peaks. From the figure, the perimeter of the ellipse is 312.3 cm; the distance between the lower and upper sample locations is 48.2 cm.



Ellipse Perimeter, $P = \pi(a + b)k$

when $a = 36.0$ cm

$b = 61.8$ cm

$$k = (1 + 1/4 m^2 + \dots), m = \left(\frac{a - b}{a + b} \right)$$

= 312.3 cm

The semi-major and semi-minor axes are taken to be half the tank radius and tank depth respectively. Since this is the longest direct path that the water particles might follow, the computed velocities should represent the highest average velocities.

The data read from the concentration verses time graphs is summarized in Table 3.5. The average times for one complete circuit of the tank are found to be 131 seconds for the 1.33 cycle per second generator frequency. The respective average travel times for the dye plumes from the lower to upper sampling location are 2.5 and 7.5 seconds. Using these values, the average water velocities for the assumed circuit can be computed:

Table 3.5 Dye Concentrations Versus Time

GENERATOR FREQUENCY (cycles/sec)	SAMPLING LOCATION NUMBER	TIME OF DYE CONCENTRATION PEAK (second after dye added)	TIME DIFFERENCE BETWEEN CONSECUTIVE CONCENTRATION PEAKS (seconds) AT EACH LOCATION	TIME DIFFERENCE BETWEEN CONCENTRATION PEAK ARRIVAL STATION 3 AND 1 (seconds)
1.33 (Expt. 2)	1	135		
			135	
		270		
		390	120	
<hr/>				
	3	105		30
		240	135	30
		375	135	15
			Average = 131	Average = 25
<hr/>				
2.13 (Expt. 1)	1	40		
		100	60	
		160	60	
		220	60	
		280	60	
	3	35	55	5
		90	65	10
		155	55	5
		210	65	10
		275	Average = 60	Average = 7.5

Wave Generator Frequency (cycles/sec)	Average Velocity (cm/sec)	
	Total Circuit	Lower to Upper Sample Location
1.33	2.4	3.4
2.13	5.2	6.4

The third dye experiment was performed to test for longer term variations of dye concentrations, possibly due to circumferential flow components in the tank. The experiment was done at the faster generator frequency. One set of water samples was taken at location 2 (Figure 3.32) at half the tank depth and half the radius. The other set was taken from location 1 near the water surface at the tank wall. The results show that after 600 seconds, there is almost no variation in dye concentration visible, and the uniform tank concentration has been achieved. No long term fluctuations of the data are evident to within the accuracy of the test.

The last dye experiment was similar to Experiment 3 except that the wave generator was operating at the lower frequency, and the sampling period was much greater. Only one set of concentration samples were obtained from location 1. Figure 3.31 shows that the dye appears to be completely mixed after 1300 seconds, and again no long term cycles variation is evident. The jump in the data at 2300 seconds cannot be readily explained. Nothing unusual was observed during the experiment. It may be the result of a calibration problem with the flourometer, although there is no reason to believe this is so.

C. Surface Drift Velocity:

Results of the experiments with the paper drifters are summarized in Table 3.6. The computed velocities for each of the tracks show that the average velocities on the tank water surface are approximately radially symmetric, at least to within about 1 standard deviation of the data. The scatter in the data can be attributed to the wave action at the tank center. Differences in mean velocity may also be due to asymmetries in the tank and wave generator installation.

Table 3.6 Surface Velocity

WAVE GENERATOR FREQUENCY (cycles/second)	PATH OF PAPER DRIFTERS (see Fig. 3.33)	AVERAGE TIME (seconds)	STANDARD DEVIATION (seconds)	AVERAGE VELOCITY (cm/sec)	VELOCITY RANGE + 1 STND. DEVIATION
1.33	A ₁ A ₂	4.2	.6	7.9	6.9 - 9.3
	A ₁ A ₃	8.9	2.1	5.5	4.4 - 7.1
	B ₁ B ₂	3.3	.44	10.0	8.8 - 11.5
	B ₁ B ₃	5.7	.95	8.6	7.3 - 10.3
	C ₁ C ₂	3.6	.62	9.3	7.9 - 11.2
	C ₁ C ₃	6.9	.89	7.0	6.2 - 8.0
2.13	A ₁ A ₂	2.6	.25	12.8	9.5 - 19.8
	A ₁ A ₃	7.1	0.9	9.0	8.6 - 9.3

An interesting feature of the surface flow becomes evident by comparing the average velocities of the drifters traveling the long paths with the velocities computed for the shorter paths. Since the measurements were all begun at the same radius, the slower velocities for the longer paths indicate that the water particles slow down as they approach the tank center. This is exactly opposite to what one would expect from continuity considerations. A possible explanation is that the momentary bursts of reverse flow from the collapsing waves slow the inflow and force it under the surface.

3.5. OIL CONCENTRATION EXPERIMENTAL RESULTS

3.5.1. Introduction

The first ten experiments have been made without the hood in place and with the wave maker operating at either 1.33 or 2.13 cycles per second. All were made with Kuwait Crude, either 60 or 120 ml, and at ambient temperatures which spanned the period from February through August. Tests were made with fresh water and sea water and documented with photographs and 8 mm movies.

Figure 3.34 shows the dimensions of the tank and sampling probe locations. Table 3.1 lists the test conditions and Table 3.2 gives the results of oil concentration verses time for the ten experiments. These results are plotted in Figure 3.35 through 3.44.

3.5.2. Observations and Results: Test 1

The first test, Test 1, was run with 60 ml of oil placed on the surface of cold fresh water. The frequency was 1.33 cps. Fig. 3.35 shows that the amount of oil entrained was the least of all the tests. The ordinate on these graphs is the percent of oil entrained $\times 10^{-2}$. It is also the concentration of the sample divided by the concentration that would exist if all the oil were uniformly distributed throughout the tank.

It is interesting to note the behavior of the oil on the surface. Fig. 3.45 shows that the oil broke up into well defined slicklets with irregular boundaries a short time, about 2 hours, after the beginning of the test. While the diameters of the slicklets were random their average length scale appeared to be about 2" or about 1/2 the wave length. Fig. 3.46 shows the irregular boundaries of these slicklets, and Figure 3.47 shows the oil eight hours after being added.

At the beginning of this test, small oil droplets, from 1 mm to 5 mm in diameter were observed. However, the observed droplets seemed to decrease in number with time and as the slicklets became more stable. While the slicklets appeared stable on the surface of the water, when they were removed, the water separated from the oil in about one hour.

Eight hours after the oil was placed on the surface the wave maker was turned off and the system was allowed to come to equilibrium. Samples were taken 13 hours after shut down and showed a negligible amount of hydrocarbons remaining in the water. The slicklets which had formed broke down into irregular shapes but still maintained their identity.

TEST 2

The only significant difference between test 1 and test 2 is the wave generator frequency which was increased to 2.13 cycles per second. A plot of concentration versus time as shown in Fig. 3.36 shows no appreciable difference from test 1. Fig. 3.48 and 3.49 show the slicklets which formed about two hours after the oil was added. Fig. 3.50 is taken

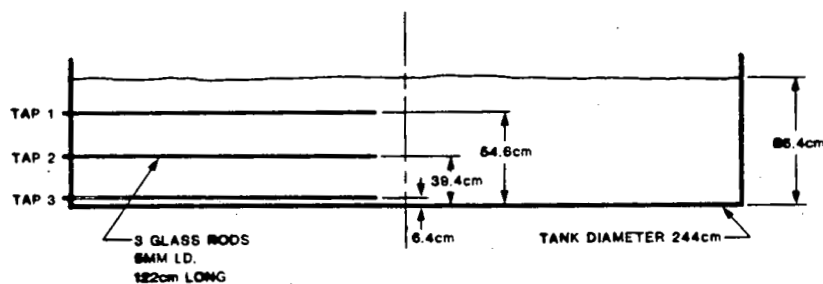


FIGURE 3.34
DIMENSIONS OF TANK AND SAMPLING LOCATIONS

CONCENTRATION VS TIME EXPERIMENT 1

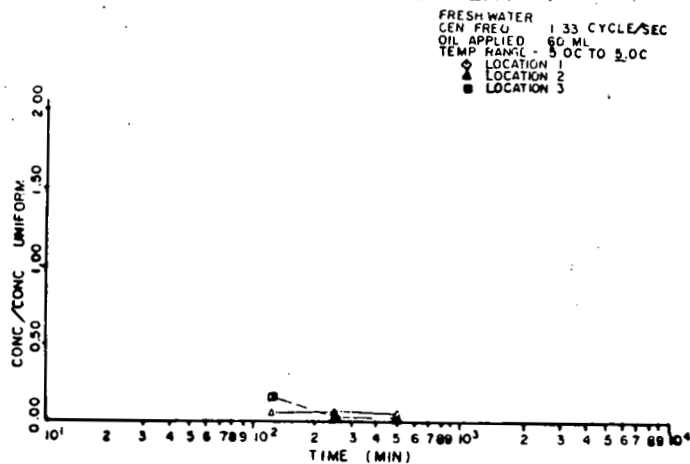


Figure 3.35. Concentration vs. Time Experiment 1

CONCENTRATION VS TIME
EXPERIMENT 2

FRESH WATER
 GEN. FREQ. = 2.13 CYCLRS/SEC
 OIL APPLIED = 60 ML
 TEMP. RANGE = 6.0 C TO 6.0 C
 ○ LOCATION 1
 △ LOCATION 2
 □ LOCATION 3

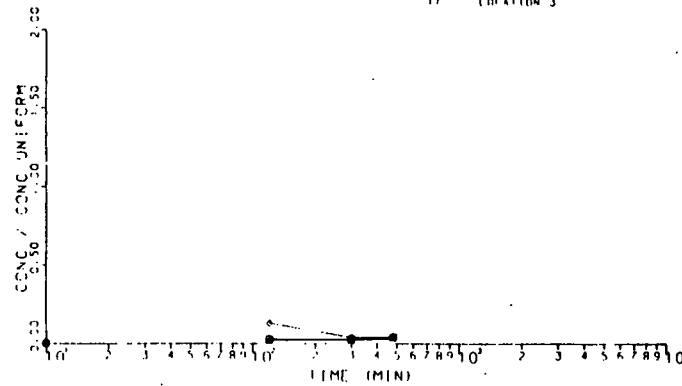


Figure 3.36. Concentration vs. Time Experiment 2

CONCENTRATION VS TIME
EXPERIMENT 3

SALT WATER
 GEN. FREQ. = 1.33 CYCLRS/SEC
 OIL APPLIED = 60 ML
 TEMP. RANGE = 15.0 C TO 16.0 C
 ○ LOCATION 1
 △ LOCATION 2
 □ LOCATION 3

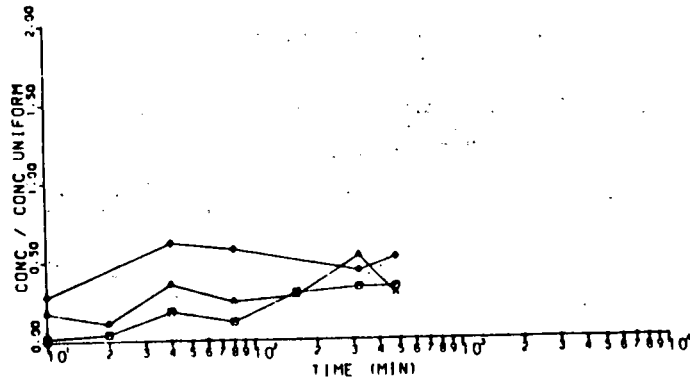


Figure 3.37. Concentrations vs. Time Experiment 3

CONCENTRATION VS TIME
EXPERIMENT 4

SALT WATER
 GEN. FREQ. = 2.13 CYCLRS/SEC
 OIL APPLIED = 60 ML
 TEMP. RANGE = 18.0 C TO 20.0 C
 ○ LOCATION 1
 △ LOCATION 2
 □ LOCATION 3

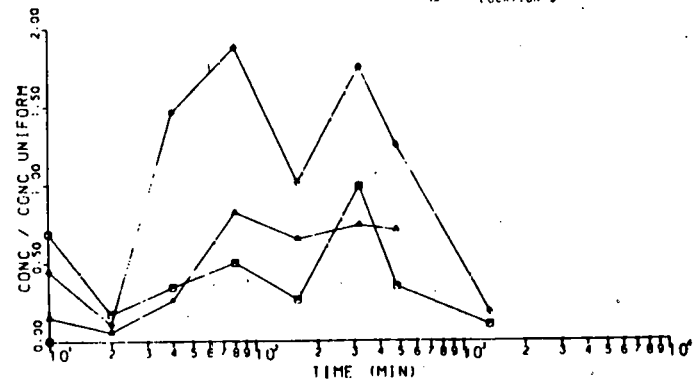


Figure 3.38. Concentration vs. Time Experiment 4

CONCENTRATION VS TIME
EXPERIMENT 5

FRESH WATER
GEN. FREQ. = 2.13 CYCLES/SEC
OIL APPLIED = 60 ML
TEMP. RANGE = 18.0 C TO 20.0 C
C LOCATION 1
A LOCATION 2
D LOCATION 3

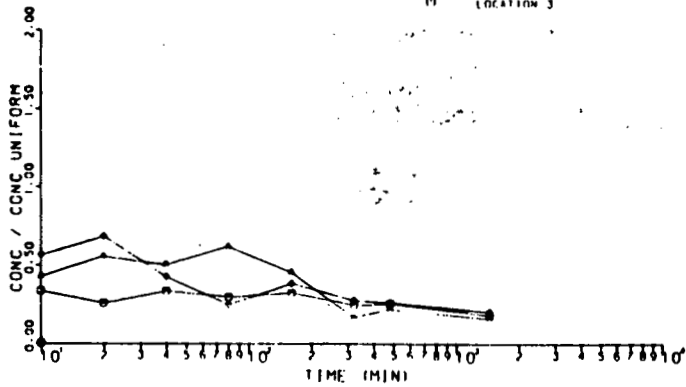


Figure 3.39. Concentration vs. Time Experiment 5

CONCENTRATION VS TIME
EXPERIMENT 6

SALT WATER
GEN. FREQ. = 1.33 CYCLES/SEC
OIL APPLIED = 120 ML
TEMP. RANGE = 22.0 C TO 23.0 C
C LOCATION 1
A LOCATION 2
D LOCATION 3

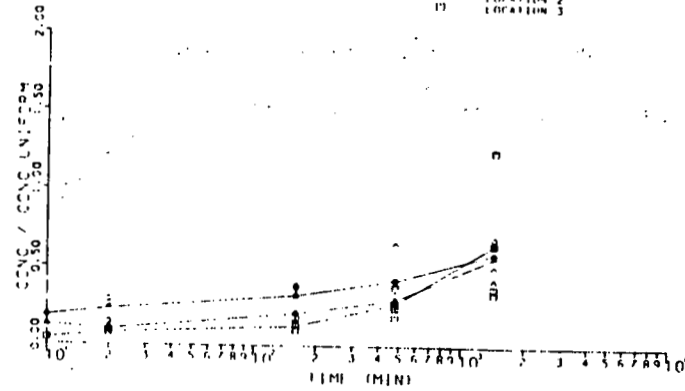


Figure 3.40. Concentration vs. Time Experiment 6

CONCENTRATION VS TIME
EXPERIMENT 7

SALT WATER
GEN. FREQ. = 2.13 CYCLES/SEC
OIL APPLIED = 120 ML
TEMP. RANGE = 20.0 C TO 22.0 C
C LOCATION 1
A LOCATION 2
D LOCATION 3

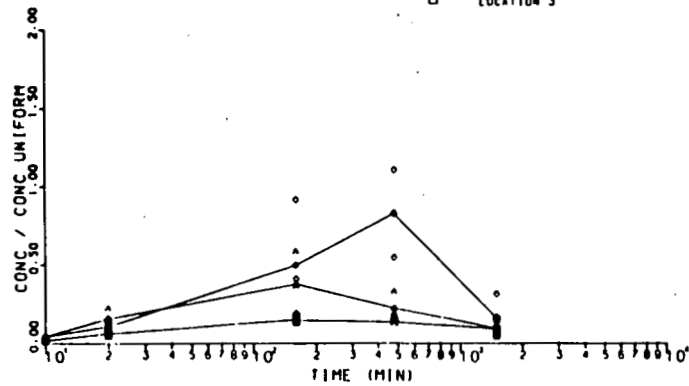


Figure 3.41. Concentration vs. Time Experiment 7

CONCENTRATION VS TIME
EXPERIMENT 8

SALT WATER
GEN. FREQ. = 2.13 CYCLES/SEC
OIL APPLIED = 60 ML
TEMP. RANGE = 20.0 C TO 22.0 C
C LOCATION 1
A LOCATION 2
D LOCATION 3

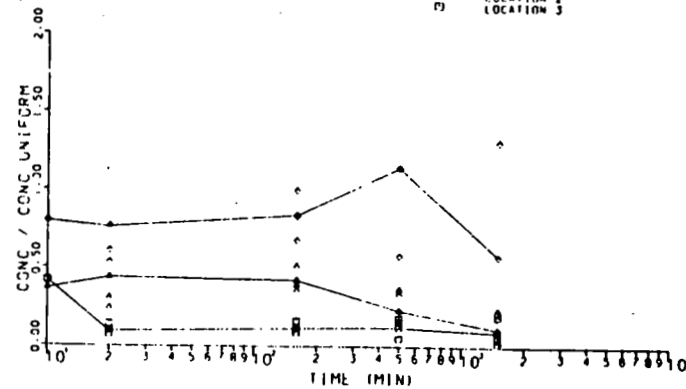


Figure 3.42. Concentration vs. Time Experiment 8

CONCENTRATION VS TIME EXPERIMENT 9

DISPERSANT APPLIED
SALT WATER
GEN. FREQ. = 1.33 CYCLES/SEC
OIL APPLIED = 60 ML
TEMP. RANGE = 25.0 C TO 27.0 C
◇ LOCATION 1
△ LOCATION 2
□ LOCATION 3

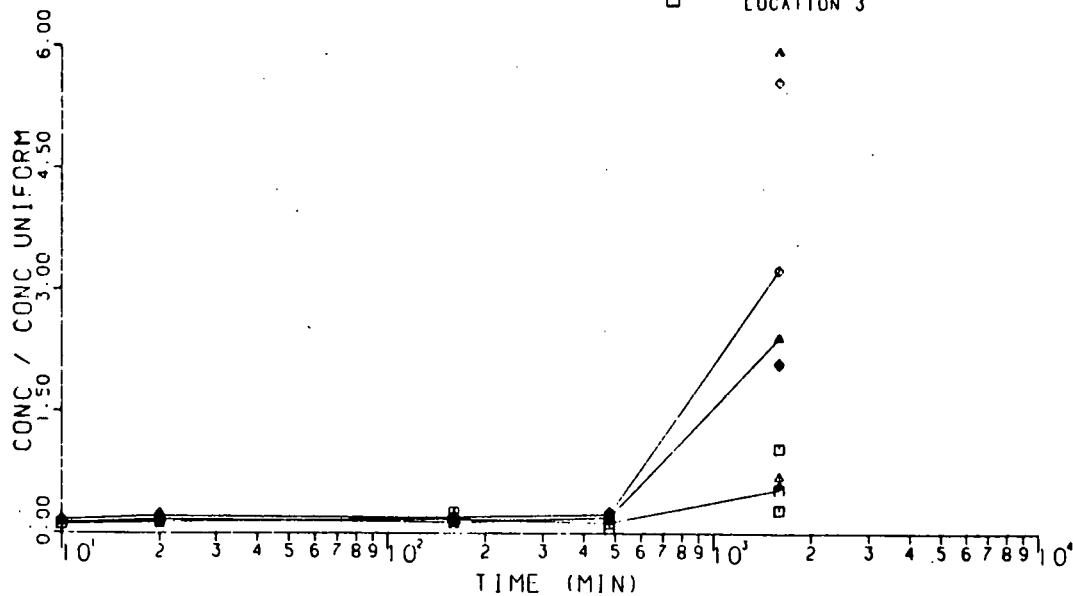


Figure 3.43. Concentration vs. Time Experiment 9

CONCENTRATION VS TIME EXPERIMENT 10

SALT WATER
GEN. FREQ. = 1.33 CYCLES/SEC
OIL APPLIED = 60 ML
TEMP. RANGE = 24.0 C TO 26.0 C
◇ LOCATION 1
△ LOCATION 2
□ LOCATION 3

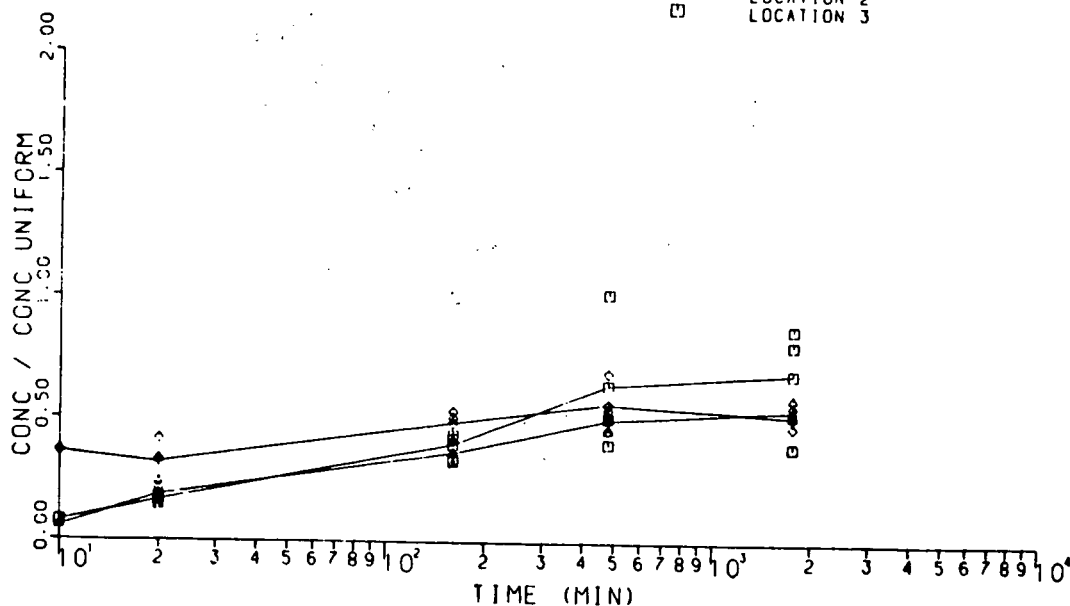


Figure 3.44. Concentration vs. Time Experiment 10



Figure 3.45. Test 1 Fresh Water



Figure 3.46. Test 1 Fresh Water

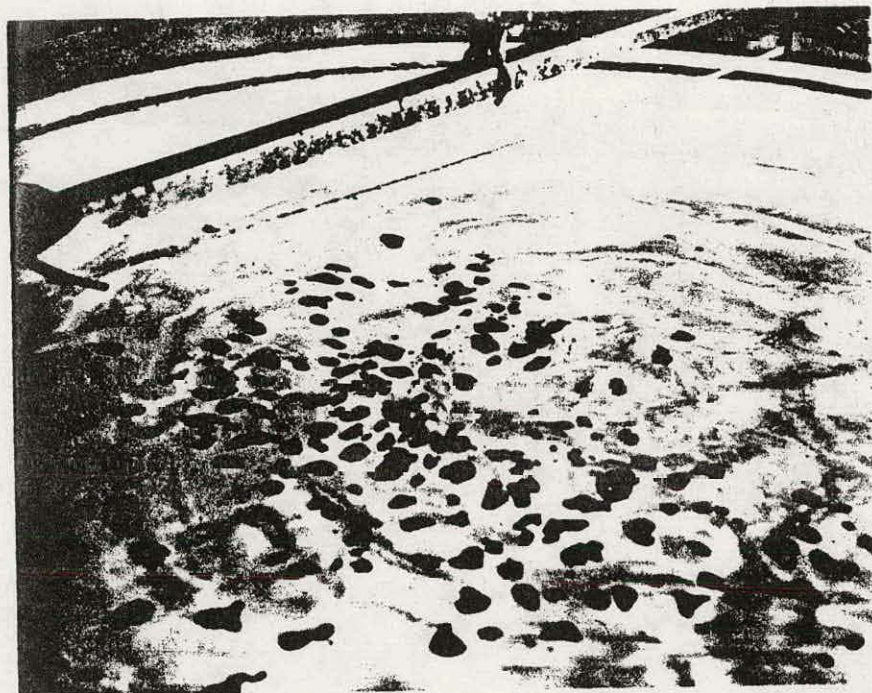


Figure 3.47. Test 1 Fresh Water Weathered 8 hours



Figure 3.48. Test 2 Fresh Water High Frequency



Figure 3.49. Test 2 Fresh Water High Frequency



Figure 3.50. Test 2 Fresh Water

from underneath the slicklets. Note that these slicklets are different in appearance to those in test 1. They show a smoother, thicker contour and are not as irregular as in test 1.

This change in appearance must be due to the difference in frequency but the reason is not apparent. Note, also, that the length scale of the slicklets do not appear to differ from test 1.

Again, the wave maker was stopped about eight hours after the oil was added and samples taken 23 hours after the oil was added show a negligible amount remaining in the water column.

Test 3

This test was a repeat of test 1 but with salt water rather than fresh water. However, the test was in June, so that the ambient temperature was appreciably higher. Fig. 3.37 shows the oil concentration in the water column appreciably higher than in the fresh water case. The concentrations do not appear to change significantly with time. The appearance of the oil on the surface was markedly different from the fresh water cases. The oil did not form the distinct slicklets as in the previous two cases but spread more uniformly and formed a cloud of small droplets underneath the slick as shown in Figs. 3.51 and 3.52 taken about 20 minutes after the oil was added. Fig. 3.53 shows the appearance 80 minutes after the oil was added. One can see discrete lumps but considerably smaller than the slicklets in the fresh water case. Fig. 3.54 shows the slick after weathering for 22 hours, and the main body of the slick is still contiguous. Fig. 3.55 shows the appearance of the oil from beneath the surface after the wave maker was stopped.

In order to check on the effect of temperature, the tank was cleaned and filled with fresh water and the conditions of test 3 were repeated. As in the previous fresh water cases, the oil broke up into slicklets as shown in Fig. 3.56. We must therefore conclude that it is the composition of the salt water that slows down the formation of slicklets.

TEST 4

Test 4 was a repeat of test 2 but with salt water. It is a repeat of test 3 but at the higher frequency. Fig. 3.38 shows the concentration of oil in the water column. They are substantially higher than in test 3 and we must conclude that the oil concentration increases with the frequency of the waves. Figs. 3.57 and 3.58 show the appearance of the slick 20 and 40 minutes after start. Fig. 3.59 shows the droplets under the slick. Fig. 3.60 shows the slick after five hours of weathering.

After about two hours of weathering, small lumps, about 1/2 inch diameter, started to form between the wave maker and the wall. An emulsion formed on the tank wall at a crack in the resin coating, and it is believed that this formed the nucleus for the lumps. These lumps would escape one at a time and migrate toward the slick at the center of the tank where they would remain as small slicklets and not join the main slick. Fig. 3.61 shows these lumps.

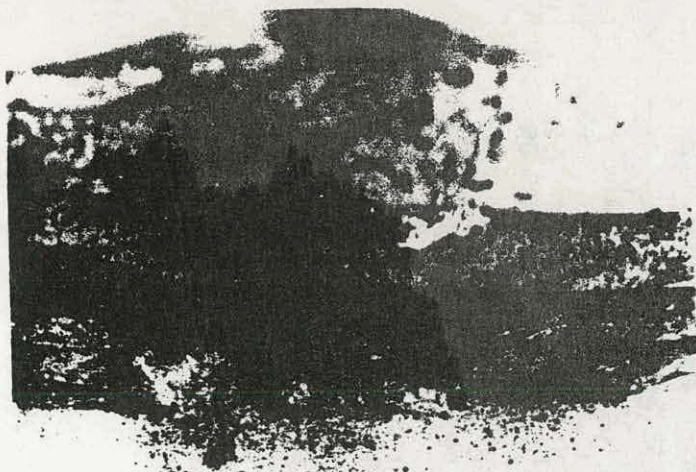


Figure 3.51. Test 3 Salt Water



Figure 3.52. Test 3 Salt Water

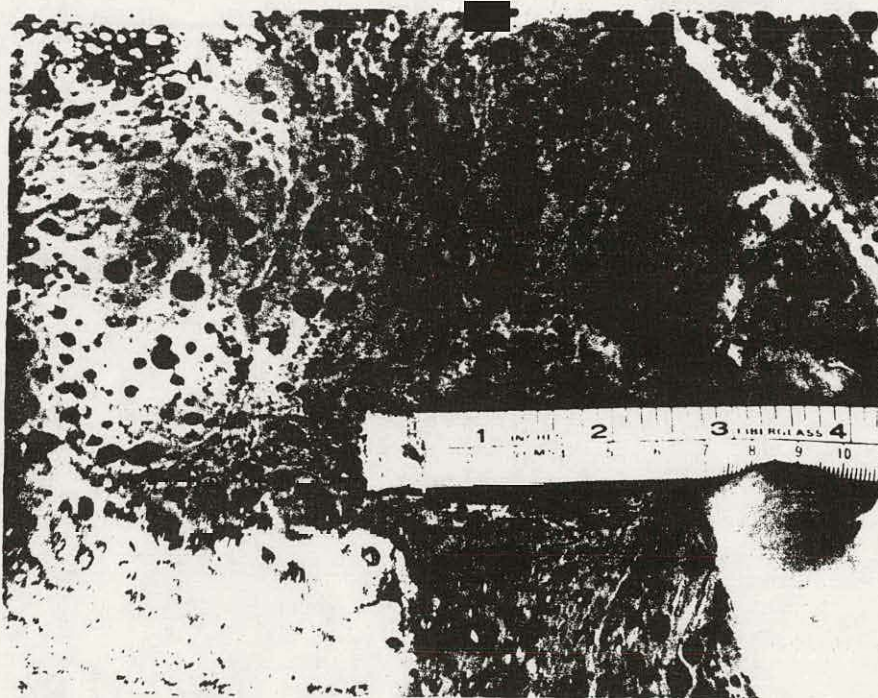


Figure 3.53. Test 3 Salt Water

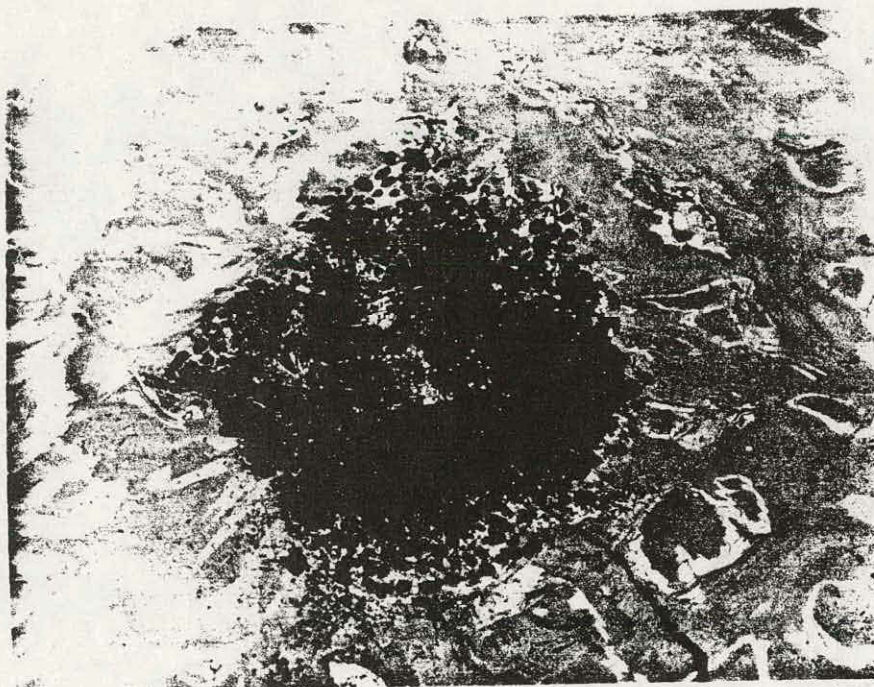


Figure 3.54. Test Salt Water Weathered 22 Hours



Figure 3.55. Test 3 Salt Water After Wavemaker Stopped



Figure 3.56. Repeat of Test 3 With fresh Water

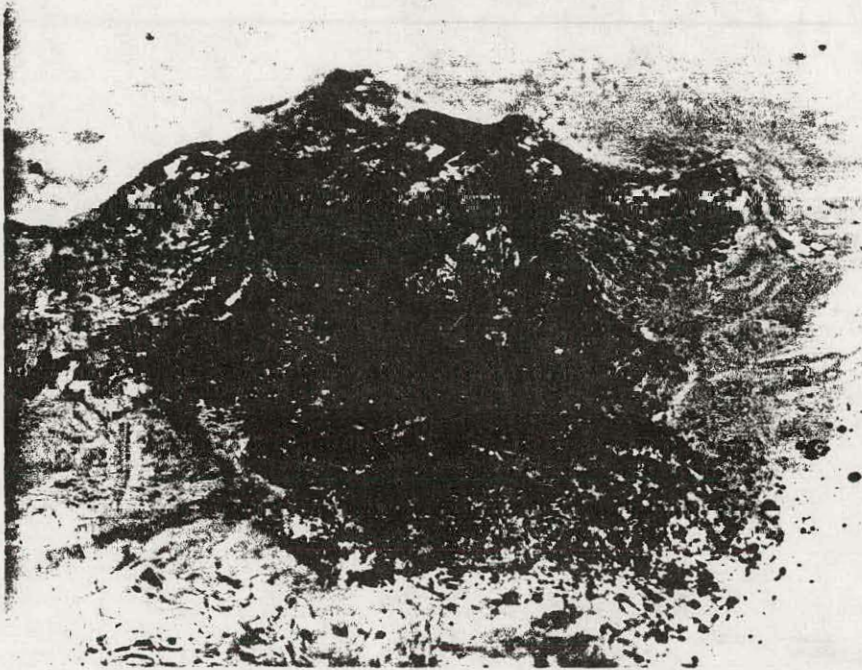


Figure 3.57. Test 4 Salt Water High Frequency

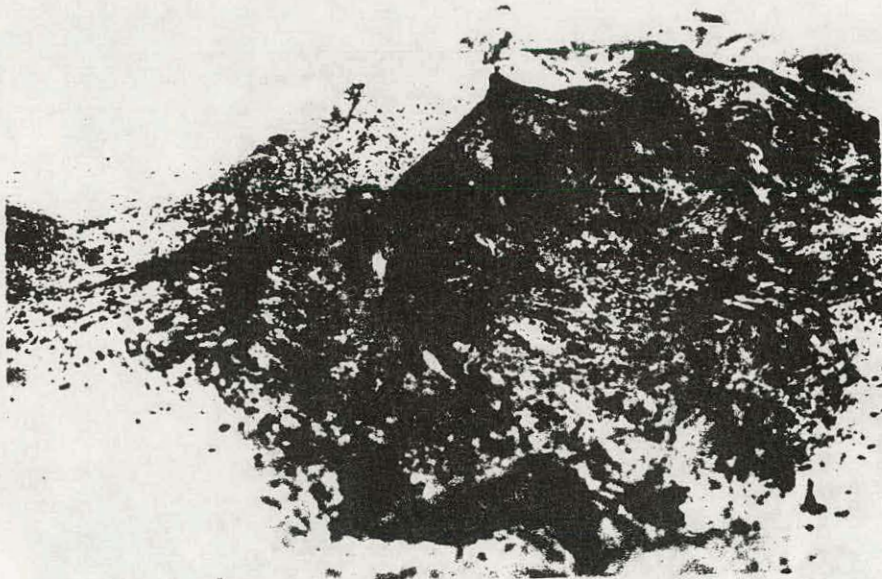


Figure 3.58. Test 4 Salt Water High Frequency

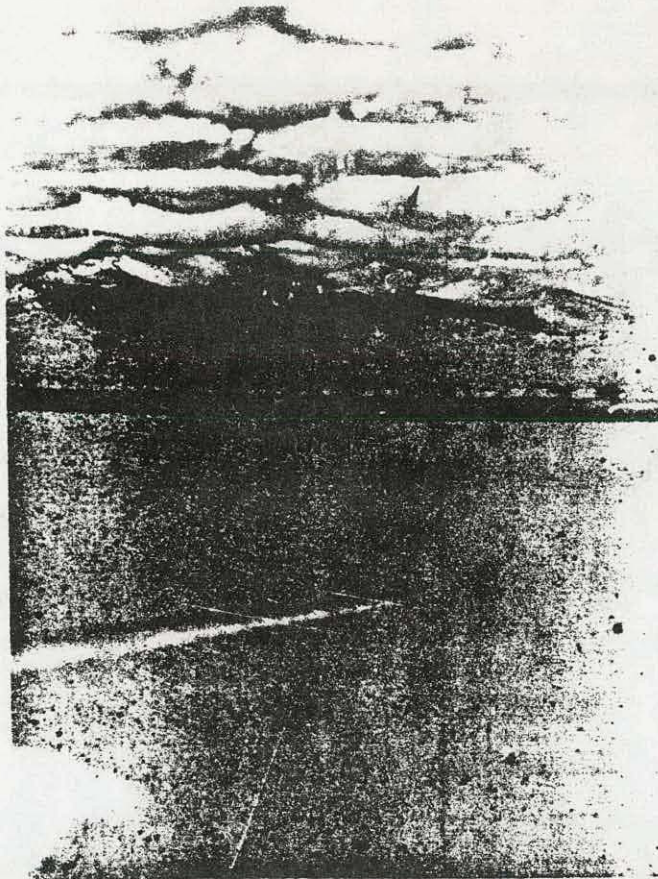


Figure 3.59. Test 4 Salt Water



Figure 3.60. Test 4 Salt Water Weathered 5 Hours



Figure 3.61. Test 4 Slicklets Forming Near Wall

After weathering about eight hours, small string-like pieces of oil could be seen circulating throughout the tank. These were approximately 1/4 mm in diameter and 3 mm long. The slick itself appeared to become an emulsion similar in appearance to chocolate mousse. Some of the tiny particles of oil would come to the surface, break and disappear into a sheen.

TEST 5

Test 5 is a repeat of test 2 but at a higher ambient temperature. Fig. 3.39 shows a higher average concentration of oil in the water column than in test 2. However, this is fresh water and the concentration is substantially lower than test 4 which has identical conditions except that it was done with salt water. It is interesting that the concentration of oil in the water appears to decrease with time in test 5. This is possibly a result of the formation of stable emulsions in the form of slicklets which float on the surface and absorb droplets that come in contact with them. As in the previous fresh water cases, these slicklets formed after about two hours and appear to become more stable with time.

TEST 6

Test 6 was the same as test 3 except that the quantity of oil added was doubled. Also, the ambient temperature was about 7°C higher. The percent concentration of oil in the water column does not appear to be significantly different from test 3. However, a noticeable increase with time is apparent and this is opposite the trend in the fresh water

tests. In Fig. 3.40, the lines are drawn through the averages of several samples taken from each port. Each data point plotted represents a single sample. Fig. 3.62 shows the appearance of the slick 20 minutes after start and Fig. 3.63 is eight hours after start. The oil has broken up and spread over the surface. The oil pieces seen appear to be aerated and not stable emulsions. The wave maker was stopped after about 24 hours of weathering and almost all the visible oil in droplet form appear to be oil covered water. The droplets range from about 0.1 mm to 2 mm in diameter. Fig. 3.64 shows the tank surface after stopping the wave maker.

TEST 7

Test 7 is identical to 6 except at higher frequency. It is the same as test 4 except the quantity of oil was doubled. Fig. 3.41 shows the concentration of oil in the water versus time. There does not appear to be a significant difference percentage wise, except possibly at the points taken just before shutdown, i.e., after 24 hours of weathering, where the concentrations at the higher frequency are lower. We note this same trend when comparing test 3 with test 4. It appears that after 24 hours of weathering, the concentration at the higher frequency decreases sharply. Figure 3.65 shows the slick 20 minutes after start and Figure 3.66 shows the slick after 24 hours of weathering. It can be seen that the weathering process has produced small slicklets of the order of 1/4 to 1/2 in. size. These are much smaller than those that appeared in the fresh water tests. The lower oil concentration after 24 hours could be a result of the stability of these slicklets and their ability to pick up oil droplets out of the water.

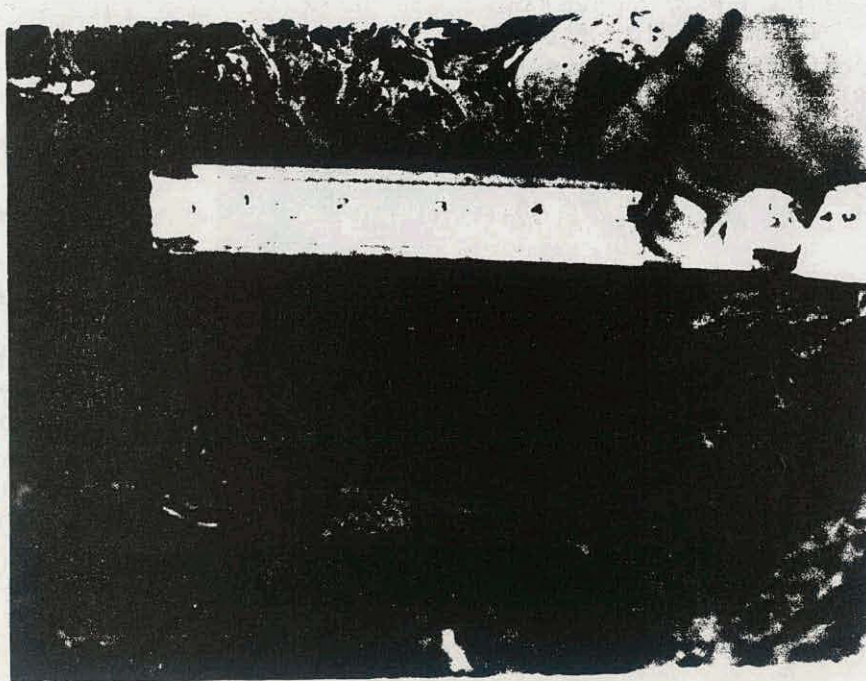


Figure 3.62. Test 6 120 ml Oil Weathered 20 Minutes

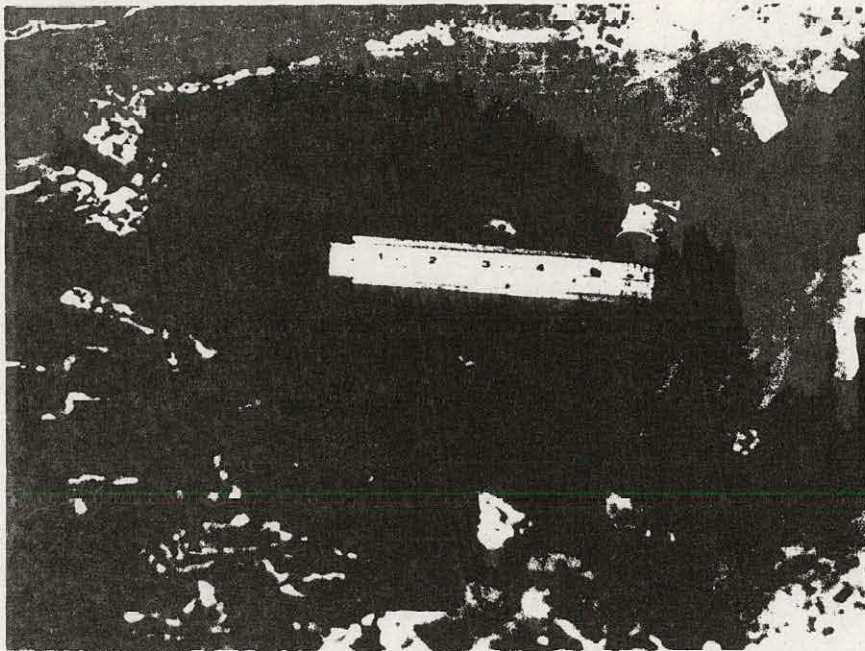


Figure 3.63. Test 6 Weathered 8 Hours

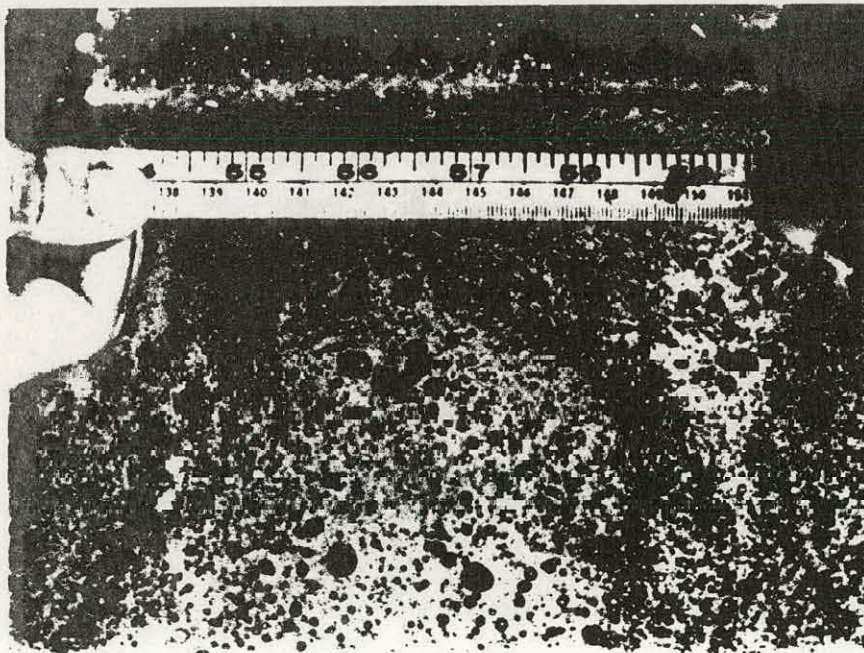


Figure 3.64. Test 6 After Stopping Wavemaker

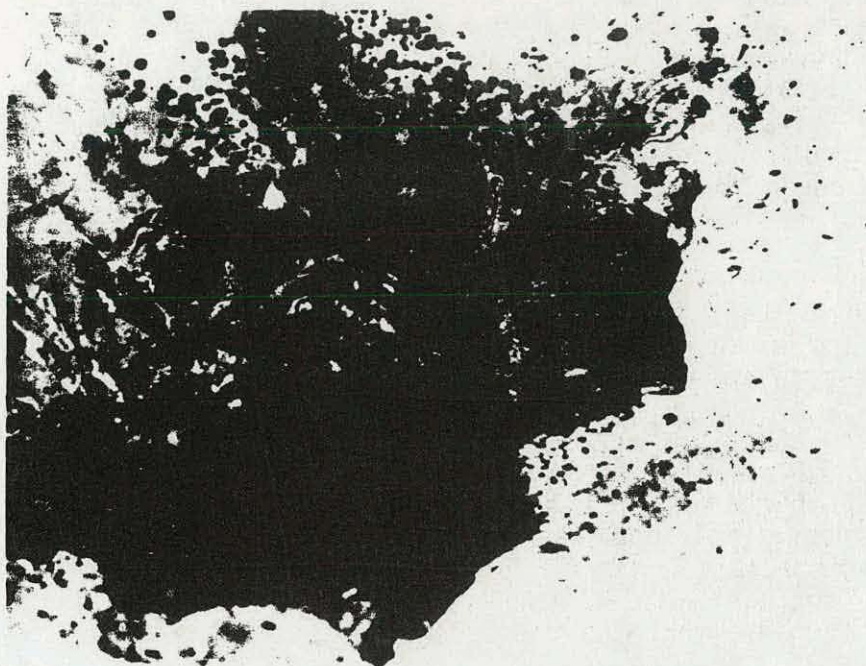


Figure 3.65. Test 7 Weathered 20 Minutes



Figure 3.66. Test 7 Weathered 24 Hours

TEST 8

Test 8 is a repeat of test 4 and similar to test 7 except with half the oil added. The concentrations shown in Fig. 3.42 appear to be higher than 7 during the early stages of the experiment, but become the same order of magnitude as the weathering continues. Again, concentration appears to increase with time, but shows a sudden drop after 24 hours of weathering. Figure 3.67 shows the slick after 24 hours of weathering and the irregular appearance of the oil is apparent. The pieces look as though they have been shredded or torn apart.

TEST 9

Test 9 was performed to test the effectiveness of the chemical dispersant Corexit 9527. The experimental apparatus was set up as usual. The wave generator was set to operate at 1.33 cycles per second and 60 ml of oil was added.

Twelve ml of Corexit mixed with 240 ml of sea water were applied to the slick immediately after the oil was added. Following the manufacturer's recommendation, the dispersant was first mixed with the tank water, keeping a water-dispersant ratio of 20:1. The mixture was then sprayed onto the water surface with a hand-held atomizer. (See Fig. 3.68). Care was taken to ensure that the dispersant contacted the entire slick.

The immediate effect of the dispersant was to submerge almost the entire oil slick. A dispersion of very fine (1 mm diameter or less) oil droplets could be seen which gave the near surface water a yellowish appearance. However, within 3 to 5 minutes, almost the entire amount of oil had returned to the surface to form a thin, opaque smooth, contiguous slick at the center of the tank (Fig. 3.69). Whenever a wave broke within the slick, a few droplets of oil would momentarily submerge as before, but they would immediately return to the surface and the contiguous slick would reform. The wave action in the tank appeared to be less violent than in previous tests. The smallest ripples were dampened out completely and the exposed water had a smooth, glossy appearance (Figure 3.70, taken ten minutes after the dispersant was added). Visible turbulent action from collapsing waves was much less. As a result, the circular wave fronts remained intact until the waves reached the very center of the tank where the constructive interference would finally cause the waves to collapse. Thus, the region of active oil submergence was very small.

Twenty minutes after the dispersant was added to the experiment, the water throughout the tank appeared mostly devoid of any oil, Fig. 3.71. Only a few very small oil droplets (again 1 mm or less) could be seen in the water just under the slick at the center. However, these were very small oil droplets, up to 2 mm in diameter attached to the underside of the slick. The oil slick developed two distinct regions: a dark contiguous glossy slick at the center of the tank, and a transparent tan film that extended out to within a few centimeters of the wave generator.

During the first eight hours, the oil slick changed very little, Fig. 3.72. During periods of relatively more intense wave action, the oil

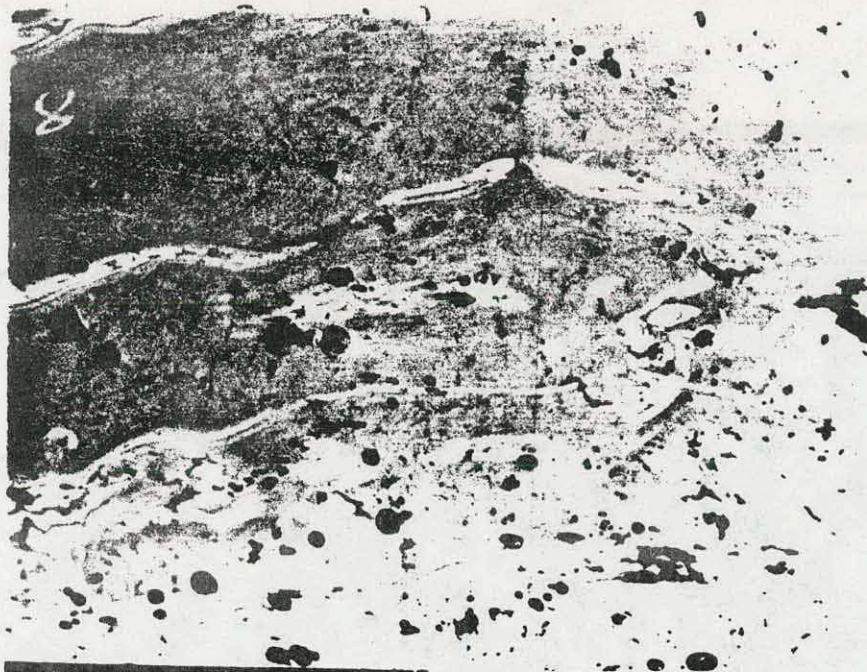


Figure 3.67. Test 8 Weathered 24 Hours



Figure 3.68. Test 9 Spraying Dispersent

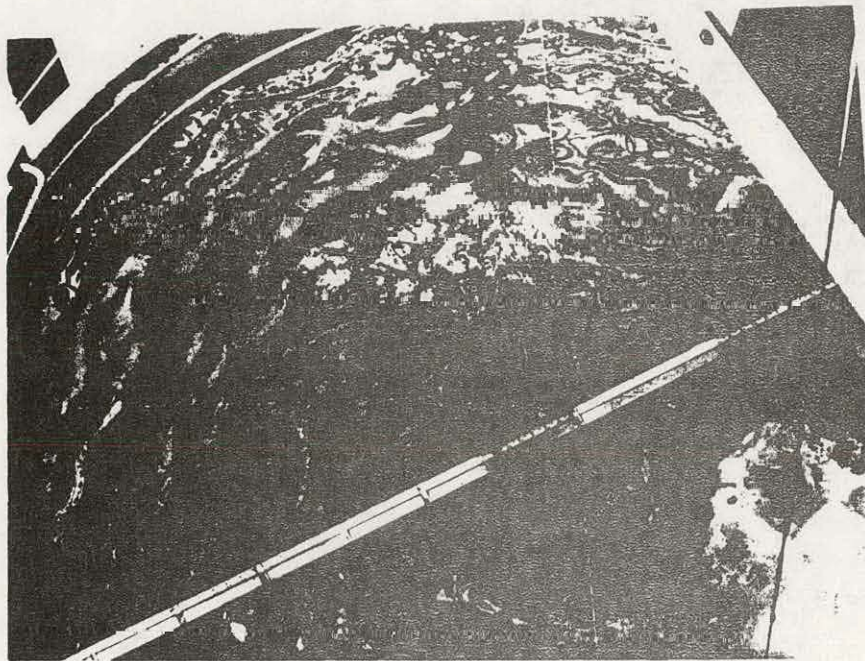


Figure 3.69. test 9 Five Minutes After Adding Dispersent



Figure 3.70. Test 9 Ten Minutes After Adding Dispersent

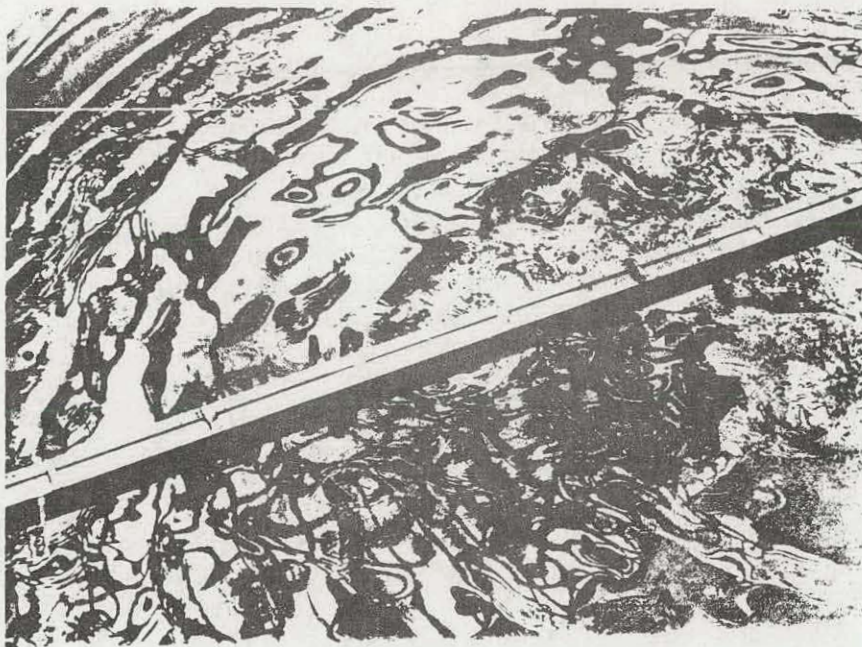


Figure 3.71. Test 9 Twenty Minutes After Adding Dispersant



Figure 3.72. Test 9 Weathered 8 Hours

near the center of the slick would break up into 1 or 2 mm size particles, but would recombine where the activity intensity lessened. Progressively more very fine oil droplets were observed in the water as the experiment progressed. However, the amount of dispersed oil continued to appear to be much less than experiments previously performed. The water remained very clear. The two distinct regions in the oil slick changed slightly. After eight hours of wave action, the center region appeared browner, similar to the color of chocolate sauce. The light brown perimeter had about disappeared and was replaced with a transparent sheen which refracted the light. Rough elongated particles of oil could be seen near the center, and some were being submerged.

The appearance of the tank the following morning after the wave generator had run for 22 hours, was radically different, Figs. 3.73 and 3.74. A very faint slick was visible on the water surface consisting of a brown film containing dark granules of oil. Most of the oil had dispersed completely into the tank in the form of small (again $< .2$ mm) dirt-like particles, although larger particles and oil droplets were also clearly visible. The water was a homogenous light yellow-brown and very murky. The waves in the tank were significantly smaller than usual, and smaller than when the experiment began. The maximum amplitude of the waves in the center was estimated to be less than 3 cm.

The wave generator was stopped 1620 minutes after the oil was added. Some of the large oil particles and droplets returned to the surface forming brown discs about 1 cm in diameter. However, most of the oil remained suspended and there was little noticeable change even one hour later. Many of the dark oil flecks appeared to be neutrally buoyant.

Ten minutes after the wave generator was stopped, 10 ml of tank water was obtained and shaken vigorously with 10 ml of CCl_4 . The fine oil droplets dissolved in the solvent as expected, but many of the small dark flecks of oil (.5 - .1 mm dia.) remained intact. Close examination of these oil particles revealed that they had the texture of asphalt. The concentration versus time plot is shown in Fig. 3.43.

TEST 10

Test 10 was a repeat of test 3 but with water about 10 C warmer. It is also the same as test 6 with 60 ml of oil added instead of 120 ml. Fig. 3.44 gives the concentration versus time curve. It shows the same magnitude and trend as tests 3 and 6. It thus appears that the normalized concentration versus time curve is not dependent on the amount of oil present in this closed system and the quantity of oil being entrained is directly proportional to the amount present. We also note that at the lower frequency the concentration keeps increasing after 24 hours in contrast to the higher frequency, when the concentration decreased markedly after the 24 hour reading.

3.6. CONCLUSIONS AND RECOMMENDATIONS

Kuwait crude oil weathers much differently in fresh water than it does in natural salt water. In fresh water, it rapidly forms slicklets which appear to be stable emulsions and very little oil gets into the water column. In the salt water tests, much more oil entered the water

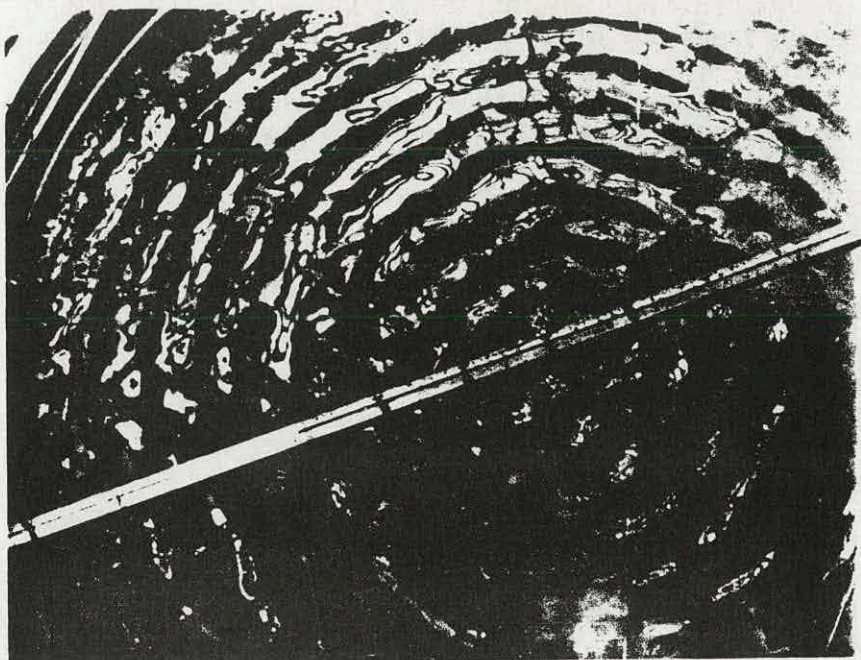


Figure 3.73. Test 9 Weathered 22 Hours

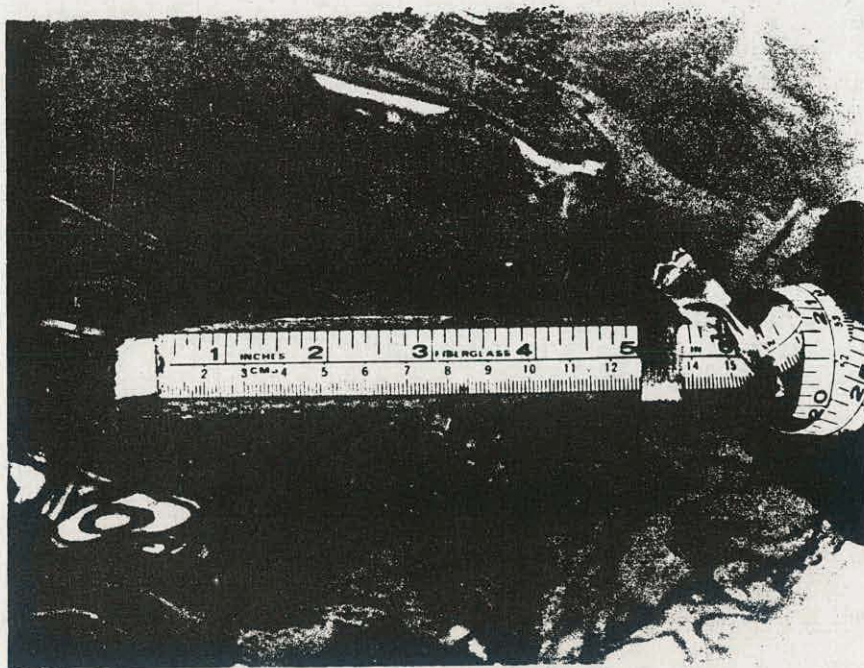


Figure 3.74. Test 9 Weathered 22 Hours

column, and this increased with time except that at the higher frequency, after weathering for 24 hours, the concentration of oil in the water column showed a dramatic decrease. This is attributed to the formation of stable emulsions that had an affinity to the droplets and took them out of the water column. The appearance of the oil in the higher frequency tests, after 24 hours showed a stringiness as though it had been shredded or torn apart. This did not happen with the lower frequency waves, where the concentration increased with time in all the salt water tests. However, it is possible that the same phenomena, the dramatic decrease in concentration, would have been observed if these lower frequency tests were run for a longer period of time. It therefore appears that the effect of increasing the frequency is to speed up the weathering process.

The effect of an increase in temperature is to increase the amount of oil getting into the water column.

Doubling the quantity of oil in the slick did not change the percent concentration of oil in the water column. This would indicate that the amount of oil getting into the water column is directly proportional to the amount present. In the ocean, currents would carry some of the oil away from under the slick.

Tests using the dispersant did not show a sudden increase in concentration of the oil in the water column immediately after adding the dispersant as might be expected. The visual properties of the slick and the waves changed, but the oil did not get into the water column until it had weathered over eight hours after adding the dispersant. After 22 hours of weathering, practically all the oil was in the water column.

The scatter in the data indicated that more tests should be made with similar conditions to improve the confidence limits. Additional tests should be made with wind driven waves and measurements taken of the rates of evaporation. Additional tests with wind driven waves and dispersants should be made.

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4.0 The Entrainment of Oil in the Water Column

Leif N. Persen

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4.1 SURVEY

4.1.1. Introduction

The present study of the entrainment of oil from a slick on the ocean's surface to the water column is mainly based on the author's idea about the process as this is explained in [1]. For the sake of completeness, this is reviewed in the next section. The present investigation is based on three experiments conducted within the framework of the Department of Energy project at the University of Rhode Island. These have been initiated and reported in the Interim Report [2] from the DOE project. It has been the present author's fortune to be allowed to influence the conduction of these experiments such that they might be used to prove or to disprove the different concepts of the entrainment. The way in which this is done will be the subject of subsequent sections.

When discussing the entrainment process, the actual quantities used to describe this process should be well defined. Thus the "entrainment rate" (\dot{m}) denotes the mass of oil transported from the slick into the water column per unit time and unit area. This quantity is not necessarily a constant. It may vary with time and location and is to be considered a local and not a bulk quantity.

4.1.2 The Entrainment Process

When an oil spill occurs, a slick is formed on the sea surface which will spread and get thinner in the process. The surface of the sea is in motion partially because of the waves, partially because of the wind-wave interaction and partially because of the current in the sea. It is known that the surface tension of the oil-sea interphase plays an important role in the entrainment process. (This is dramatically exhibited by adding a dispersant to an oil slick and thereby reducing the surface tension whereupon an enhanced entrainment is observed.)

It is furthermore recognized that the mechanical agitation that takes place at the sea surface plays an important role in the process. This may lead to the identification of the energy input at the surface as a second important parameter. Realizing however that this energy input may take place in different manners with different results as far as the entrainment process is concerned, one is led to the conclusion that additional parameters must be identified.

Preliminary experimental evidence seems to indicate the following scenario. The mechanical agitation will produce "entrainable" particles of oil mainly when it causes rifts in the oil film, i.e., when the "premissible" surface tension is exceeded. An analogy may be found in the production of fiber particles when tearing a sheet of paper. If that concept is correct, the production of entrainable particles is to be considered a random process even under the most well-defined conditions. Bearing in mind the conditions on the open sea, one will conclude that the production of entrainable oil particles must indeed be considered a random process. One must, however, also be permitted to assume that the average or mean production may be quantified in the same way as mean

values in turbulent fluid flow are determined. A support for such an idea may be found in the following observations:

1. The addition of a dispersant makes it easier to produce such rifts, thus enhancing the production of entrainable particles.
2. The production of entrainable particles will appear to be greater at the locations where the oil slick on the surface is thin than where it is thick or perhaps in the form of an emulsion (mousse). This is in complete agreement with observations previously made.

The expression "entrainable" particles needs some extra comments. The violent actions of breaking waves have been widely accepted as the action responsible for the entrainment of oil in the water column.* Such action produces oil particles of different sizes and the larger ones are by the action of buoyancy forces, quickly returned to the surface. The smaller the particles, the easier it is for them to be carried by the mean flow in the upper part of the water column. Thus, the term "entrainable" particles is reserved for those oil particles (or oil covered water droplets) which are "trapped" by this motion. The violent action of breaking waves can only force oil into the water column to a certain depth, the order of magnitude of this depth being the wave height. Thus, the entrainment of oil in the water column is very much dependent on the re-circulating motion connected with the waves in the upper layers of the water column. (It should be emphasized that the concept of "entrainable" particles makes entrainment possible also in the absence of breaking waves.)

There is, however, also another type of re-circulating flow in the ocean which is caused not by the wave motion, but by the non-uniform horizontal velocity distribution in the direction of the wind. This type of re-circulating motion will bring the entrained oil particles down to depths which are orders of magnitude larger than those in the previous cases. This type of motion can be modeled analytically on the turbulent plane jet flow or on the turbulent boundary layer type flow. This will be shown subsequently.

The picture given here of the entrainment envisages a semi-steady case in which a certain amount of oil is trapped by a re-circulating type of flow. If the conditions on the surface change, the amount of entrained oil will change. Assume, as an example, that the surface became completely calm, and that the re-circulating flow died out completely. Then only the extremely small droplets of oil which could be held in suspension would remain "permanently" entrained in the water column, the rest of the oil would resurface (or some might sink due to change in physical properties).

*See [3] Phani P.K. Raj: "Theoretical Study to Determine the Sea State Limit for the Survival of Oil Slicks on the Ocean" Final Report, No. Cg-D-90-77, Task No. 4714-21. Department of Transportation, U.S. Coast Guard, June 1977. p. 4-9

A consequence of the given description of the entrainment process is the fact that the so-called entrainment rate at the surface can no longer be considered a quantity determined by surface conditions alone. (Energy input, etc.). It is intimately connected with the re-circulating flow in the sea. As a further consequence, the search for "new" parameters to describe the entrainment rate will have to be replaced by a search for a more or less semi-empirical description of the recirculating flow from which the entrainment rate can be deduced.

One may, as a matter of fact, envisage a mechanism whereby the effect of the mechanical agitation that takes place at the surface (waves, breaking waves, raindrops, wind, etc.) is mainly to produce an adequate supply of entrainable particles in the immediate neighborhood of the surface. How many of the entrainable particles will be trapped by the re-circulating flow is then determined by the "strength" of this flow (whereby the strength of this flow will subsequently have to be defined in more exact terms).

One may contemplate this situation somewhat further. If the re-circulating flow is steadily "trapping" new particles, average concentration of oil in the region of this re-circulating flow must be steadily increasing. If it is not, i.e., if a semi-steady state is reached, the concentration will be constant and the entrainment rate zero. This can only occur in two cases. In the first case, there is no more production of entrainable particles at the surface, a situation that may well be feasible in view of the changes that the oil undergoes as it is being weathered on the surface. In the second case, an adequate supply of entrainable particles is present in the surface layer, but the re-circulating flow is returning formerly trapped particles at the same rate as new ones are being trapped.

The entrainment process described above has made no mention of the fact that the oil changes as it stays on the water surface and is being mechanically treated, a fact that is frequently referred to as "weathering" of the oil. Well known features of this process are the evaporation of the lighter components of the oil and the formation of chocolate mousse in some cases. It is evident that these processes will influence the composition of the entrained oil. Thus, it is already clear from the start that the entrained oil is different from the originally spilled oil, a fact that becomes important in the experimental investigation of the entrainment process.

4.1.3 Scope of the Experimentation

The entrainment process is a very complex one, not only because of the complexity of the surface conditions, but perhaps even more by the fact that the boundary conditions for the process change both with time and space. This may perhaps best be illustrated by observing that at one particular instant the situation downstream of a source continuously feeding a slick can be subdivided into several regions in which different predominant conditions prevail:

1. Immediately after the source, the oil is in its virgin state, but in this region is rapidly being changed due to evaporation of its lighter components.

2. The first region is overlapped by the second in which the situation is described in an undated report by the JBF Scientific Corporation (no identified author) for the American Petroleum Institute, p. 37:

"One of the important physical characteristics of crude oil slicks which is often neglected in the literature is the existence of one or more thick oil patches surrounded by a thinner film of oil. These thick areas have been referred to as 'lenses' or 'globs'. Investigators who have considered such thick patches report that they may contain 90% of the total oil in the slick, and that the patches are normally several millimeters thick as opposed to thousandths of a millimeter for the thinner surrounding film."

"Under conditions of no wind, the slick most probably spreads radially from the lens. However, in the presence of wind and waves, the radial spreading from the leading edge is continually overrun by the higher-velocity lens. The wind and wave activity cause the lens to break up into long windrows, each of which continues to act as a generator or reservoir of oil."

Most probably the important amount of entrained oil is coming from the thin film surrounding the lenses.

3. The next region which may be identified is the one in which "chocolate mousse" is being formed. According to the same report:

"Patches of 'chocolate mousse' should be conceptually distinguished from the lenses, because lenses appeared immediately after the oil was spilled and tended to remain roughly circular while 'chocolate mousse' was formed some time later and became elongated in windrows during the tests."

4. The last region to be specified is so far downstream of the source that the weathering of the slick is more or less complete in the sense that further changes do not take place. The formation of tar balls is starting and the slick seems to be more or less disintegrated.

It is clear that with boundary conditions as complex as those described above, the entrainment process is not easily accessible to analytic treatment. A study of the process should, therefore, start with experimentation under clearly identified and simplified boundary conditions.

The way in which the entrainment process has been visualized in the preceding section has reduced the importance of a detailed analysis of droplet formation at the slick. The main importance is now placed on the re-circulating motion and its ability to "trap" the droplets which presumably are being produced in adequate quantities. This production can

be related to certain input data characterizing the surface conditions, and it is emphasized that now the overall (bulk) production is being at the center of interest, not the details of droplet formation.

If one is faced with the problem of designing experimental set-ups which would give adequate information on the droplet formation, one would most probably have to consider a so-called "semi-steady" situation whereby the net bulk entrainment rate is zero. A change in the surface situation which could be achieved without changing the re-circulating motion could, through measurement of the concentration of oil in the water column, be interpreted to give information on the droplet production.

Because this experiment is such that the surface conditions and the re-circulating motion can be manipulated separately, the experiment will allow for a study of the "trapping" mechanism of the re-circulating motion. Thus, an adequate quantification of what is previously called the "strength" of this motion can be made. The "raindrop experiment" to be considered in detail later, is just an experiment of the type mentioned above.

The situation where the re-circulating motion is caused directly by the local wind-wave interaction at the sea surface is to be studied in the so-called "wind-wave experiment". Since the re-circulating flow is being monitored, the possibility of relating the results from this experiment to the others is present.

The situation which arises when the re-circulating motion dies out is to be studied in the so-called "drop size experiment". This experiment also provides the opportunity to study the entrainment from a slick exclusively driven by the turbulent motion in the sea (connected with the re-circulating flow).

4.1.4 The Drop-Size Experiment

This experiment was originally conceived of and conducted by Dr. T. Kim and Mathew Cherian. The first results were reported in detail in [2] where the major emphasis was placed on the influence of interfacial tension on drop size. The apparatus used is shown in Fig. 4.1 and consists mainly of a cylindrical tank and a centrally mounted impeller which can be operated at different angular velocities. The tank is filled with sea water on the surface of which a certain amount of oil is poured. To prevent the whole content of the tank from rotating with the impeller, the tank is supplied with baffles.

At very high angular velocities (of the impeller), the oil is almost totally "whipped" into the water column. Depending both on the angular speed and on the length of time when the impeller is run, different concentrations of oil in the water column are observed as a function of the time elapsed since shut off of the impeller. This result may be correlated with drop-size measurements. The fact that a certain portion of the entrained oil seems to remain "permanently" in the water column may be the most important part of the entrainment from a biology standpoint because it allows for a long term influence of the oil on marine life.

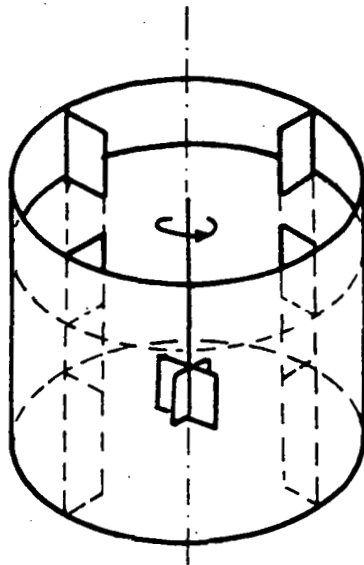


Fig. 4.1 Apparatus for the Drop-Size Experiment

The same arrangement may, however, be used to study entrainment from a slick due exclusively to small scale turbulent motion underneath it. In this case, no mechanical agitation due to waves or rain, etc. takes place at the surface. The speed of the impeller is small, and the effect of the baffles is to more or less break up the horizontal rotation of the fluid. A special type of flow, in which vortices starting out from the surface can be identified, is produced and since the flow field can easily be monitored, the entrainment process under these special circumstances can be related to the observed entrainment in the other experiments. Whatever quantity related to and characterizing the flow is best suited as a relating parameter to the entrainment, will emerge as a result of the investigation.

4.1.5 The Raindrop Experiment

This experiment was first conceived of and conducted by Dr. Peter Cornillon and the results were reported on in [2]. The geometry of this experiment is shown in Fig. 4.2 where the "rain" is produced as drops falling from the needles in the bottom of the *B* container and is falling onto the water surface of the container *C*. On this surface, an oil slick is being placed and one has an arrangement whereby the mechanical agitation at the surface can be manipulated by adjusting the "intensity" of the rain, i.e., by changing the kinetic energy per unit area of the impacting raindrops. In its original form, as conducted by Dr. Cornillon no re-circulating flow was created. The apparatus has been changed by

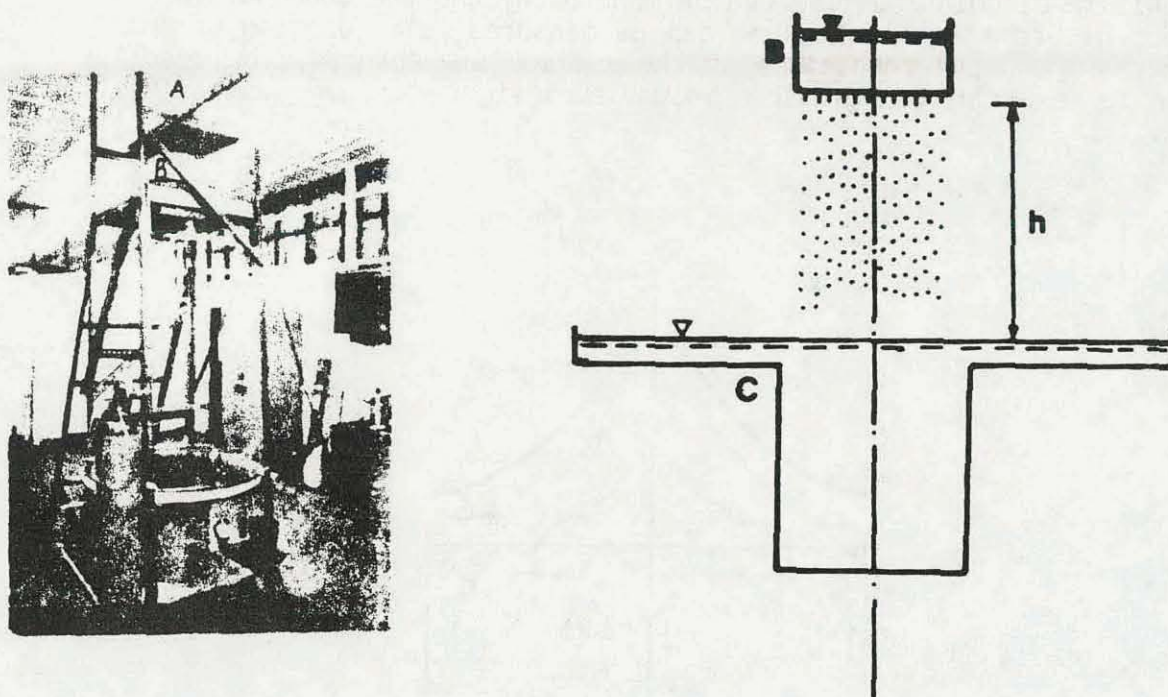


Fig. 4.2 Sketch of the Raindrop Apparatus

the introduction of an impeller and baffles of the same type as in the drop-size experiment. In this way provisions have been made to create the same type of small scale turbulent motion underneath the slick as in the first experiment, and the influence of the mechanical agitation at the surface can thus be experimentally explored. It should be mentioned that the initial experiments with this apparatus have shown that with no re-circulating motion in the water column, entrained oil in the water column is not found below the immediate layer underneath the slick. This is in complete agreement with the concept of the entrainment process already outlined in the Introduction, and may be considered as experimental support for the concept.

4.1.6 The Wind-Wave Experiment

This experiment was originally conceived of by Dr. Rodger Dowdell and was conducted by Steven Parks (see Section 3). The arrangement is shown in Fig. 4.3. A circular tank *A* is filled with water on the surface of which an oil slick may be applied. A doughnut shaped wave-maker *C* is shown close to the surface and by agitating this doughnut vertically at different frequencies and/or amplitudes, a pattern of radially moving surface waves may be created. In addition, a hood may be placed over the surface and by suction applied to the top of the hood *B*, a radially directed wind over the surface is created. The shape of the hood is such that the wind is of constant velocity. The arrangement seems to be well suited for a study of the wind-wave interaction and the influence on the

oil slick of this action. The wave action as well as the wind action will create a re-circulating flow as shown in the sketch, Figure 4.3. Since this re-circulating flow can be monitored, and the concentration of entrained oil in the water column can be measured as a function of space and time as the input conditions on the surface are changed, the results from these experiments provide valuable insight to the entrainment process.

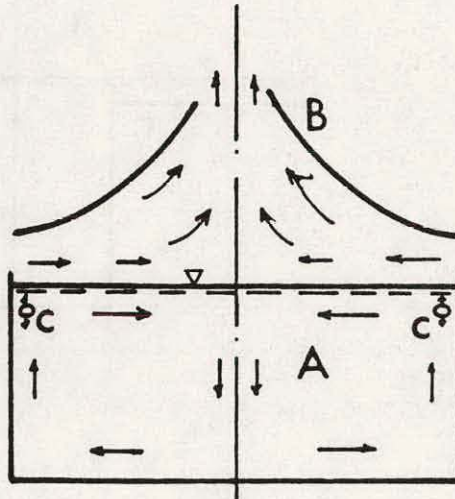


Fig. 4.3 The Wind-Wave Experiment

4.1.7 Experiment-Reality Correlation

The presentation of the experimental efforts has put the emphasis on the re-circulating flow underneath the slick as a common feature of all experiments whereby the different phases of the entrainment process are being studied. If these experiments are being properly executed, and provided the proper range of variation of the input data can be achieved, they present a range of conditions which cover most of those occurring along the slick as described in Section 4.3. Even the production of chocolate mousse can be expected to occur in the wind-wave experiment.

If, however, this information is going to be applicable to the real life situation at sea, the re-circulating flow which occurs at sea will have to be ascertained. This can be attempted experimentally by proper in-situ experimentation. Most probably one will find that the re-circulating flow connected with the waves can be experimentally explored, but that the very large scale motion connected with the non-uniform horizontal velocity of the surface layers cannot.

This, then is the point at which the re-circulating large scale motion may be theoretically explored through an analytic approach using

the method described by Leif Persen [4] and applied successfully to turbulent boundary layers. It should be mentioned that this approach does not include the influence of a possible thermal stratification in the ocean, but it will be sufficient as a first approximation. A later sophistication of the approach may be attempted when deemed necessary.

4.2 THE RECIRCULATING FLOW IN THE OCEAN

4.2.1 Introduction

The flow in the upper layer of the ocean will, where there is a gradient in the horizontal direction of the wind, exhibit a horizontal velocity which varies with the distance in the horizontal direction. This will give rise to a vertical motion of the fluid which goes to large depths compared with the wave heights. It is this motion which is responsible for the entrainment of oil particles at large depths. In the present section this motion is modeled on similar turbulent flows, i.e., flows which exhibit a change in the magnitude of the main velocity component with a correspondingly induced transverse velocity component which will then be responsible for a spreading effect. It is a fact that if one limits the scope to two-dimensional cases, such turbulent flows exhibit similarity properties of some kind, and it is easy to imagine this feature carried over to the turbulent flow in the upper part of the ocean.

The present approach will consist of an examination of the two-dimensional boundary layer flow and the two-dimensional jet flow in order to prepare the path for an examination of the fate of oil droplets in such flows. It will also show how these situations are relevant to the flow in the ocean.

4.2.2 The Turbulent Boundary Layer

The flow in the turbulent boundary layer on a flat plate may be described in a simplified way by assuming the existence of a law of the wall: [4]

$$u^+ = f(y^+) \quad (2.1)$$

or

$$y^+ = \phi(u^+) \quad (2.2)$$

The essence of this law is that the turbulent flow is such that it prescribes a one-to-one correspondence between the non-dimensional wall distance y^+ and the non-dimensional velocity u^+ parallel to the wall. It should be noticed that these quantities are defined as

$$u^+ = \frac{\bar{u}}{v_*}, \quad y^+ = \frac{yv_*}{\nu} \quad (2.3)$$

where

\bar{u} = mean velocity parallel to the wall (x-direction)

\bar{v} = mean velocity perpendicular to the wall (y-direction)

x = coordinate along the wall

y = coordinate perpendicular to the wall

v_* = shear velocity = $\sqrt{\tau_w/\rho}$

τ_w = shear stress at the wall

ρ = density of the fluid

ν = kinematic viscosity of the fluid

The mathematical problem of solving the basic equations and seeking the implications of the statement in (2.1) are shown in detail in [4], and only some results need to be drawn upon here:

- 1) The variation of the shear stress τ in the fluid is given as

$$\frac{\tau(x, u^+)}{\tau_w} = 1 - \frac{G(u^+)}{G(\xi)} \quad (2.4)$$

where

$$G(\xi) = \frac{1}{3}\xi^3 + \frac{A}{\kappa^2} \left[e^{\kappa\xi} [(\kappa\xi)^2 - 2\kappa\xi + 2] - 2 - \frac{1}{3}(\kappa\xi)^3 - \frac{1}{4}(\kappa\xi)^4 - \frac{1}{10}(\kappa\xi)^5 - \frac{1}{36}(\kappa\xi)^6 \right] \quad (2.5)$$

Here ξ is the value of u^+ at the outer edge of the boundary layer, i.e.

$$\lim_{y \rightarrow \delta} u^+ = \xi = \frac{U_0}{v_*} \quad \lim_{y \rightarrow \delta} y^+ = y_0^+ = \frac{\delta v_*}{\nu} = \phi(\xi) \quad (2.6)$$

and y_0^+ is the corresponding value of y^+ . The constants A and κ have been determined by D.B. Spalding [5]: $A = 0.1108$, $\kappa = 0.4$.

2) The vertical velocity \bar{v} is given as

$$\bar{v} = -\frac{\nu}{v_*} \frac{dv_*}{dx} y^+ f(y^+) \quad (2.7)$$

3) The solution to the problem renders ξ as a function of x :

$$G(\xi) \frac{d\xi}{dx} = \frac{1}{\nu} U_0 \quad (2.8)$$

where as before U_0 denotes the constant outer velocity. Through a combination of (2.7) and (2.8) it is now possible to establish the following equation for \bar{v} :

$$\bar{v} = U_0 \frac{y^+ f(y^+)}{\xi G(\xi)} \quad (2.9)$$

and at the outer edge of the boundary layer the limiting value \bar{v}_∞ is obtained

$$\bar{v}_\infty = U_0 \frac{y_0^+ f(y_0^+)}{\xi G(\xi)}$$

Since (2.8) gives the relationship between ξ and Re_x one may use ξ to indicate a certain position along the wall:

$$Re_x = \frac{U_0 x}{\nu} = \int_0^\xi G(z) dz \quad (2.10)$$

Then the relation (2.9) may be interpreted as a variation of \bar{v} at a given position x (given through ξ) as y varies from zero (at the wall) to y_0^+ (at the outer edge of the boundary layer). The implication of the law of the wall is however that (2.9) also describes the variation of \bar{v} at a given value of y as x varies. This is schematically shown in Fig. 4.4 where $y = \text{constant}$ is shown to

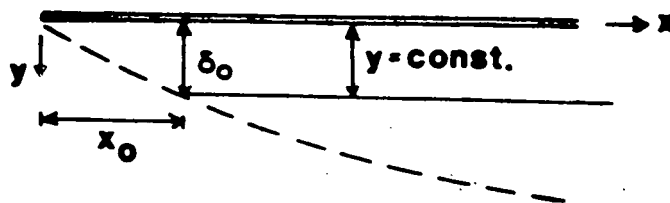


Fig. 4.4

hit the outer edge of the boundary layer at $x = x_0$. The corresponding value of ξ is ξ_0 and at this point the vertical velocity \bar{v} is from (2.9) found to be

$$\bar{v}_0 = U_0 \frac{y_{0,0}^+ f(y_{0,0}^+)}{\xi_0 G(\xi_0)} \quad (2.11)$$

where now $y_{0,0}^+$ represents the value of y_0^+ at $\xi = \xi_0$. Since ξ is related to the local Reynolds number Re_x through (2.10) it is observed that the lowest value for Re_x for a given value of y is

$$Re_{x_0} = \frac{U_0 x_0}{\nu} = \int_0^{\xi_0} G(z) dz \quad (2.12)$$

It is now easily shown that for a given value of y the variation y^+ as one progresses in the x -direction is given as follows:

$$y^+ = \frac{y v^*}{\nu} = \frac{y U_0}{\nu} \frac{1}{\xi} \quad (2.13)$$

where the variation of x is expressed through ξ . Since this starts to be valid at $x = x_0$ one has (since the constant value of y equals δ_0)

$$y_{0,0}^+ = \frac{\delta_0 v_*}{\nu} = \frac{y U_0}{\nu} \cdot \frac{1}{\xi_0} \quad (2.14)$$

Thus the variation of y^+ with x (or ξ) will be:

$$y^+ = y_{0,0}^+ \frac{\xi_0}{\xi} \quad (2.15)$$

Finally, it has been shown [6] that the shear stress τ can be expressed as:

$$\frac{\tau}{\rho U_0^2} = \frac{1}{\xi^2} \left[1 - \frac{G\left(\frac{\bar{u}}{U_0} \xi\right)}{G(\xi)} \right] \quad (2.16)$$

and the stream function Ψ may be given as

$$\Psi = \int u \, dy = \int u^+ v_* \, dy = \nu \int u^+ \, dy^+ = \nu \int u^+ \frac{d\phi}{du^+} \, du^+ \quad (2.17)$$

Using D.B. Spalding's formulation [5] one will get:

$$\Psi = \nu \left[\frac{(u^+)^2}{2} + A \left(e^{\kappa u^+} (\kappa u^+ - 1) - (\kappa u^+)^2/2 - (\kappa u^+)^3/3 - (\kappa u^+)^4/8 - (\kappa u^+)^5/30 \right) \right] \quad (2.18)$$

This ends the exhibition of the implications of a turbulent boundary layer. It is not accurate, the procedure used has been improved, but for the present purpose it ought to be sufficient.

4.2.3 The Flow in the Upper Layer of the Ocean

The flow in the ocean is turbulent and this is also the case in its upper layer. In this layer however, surface waves are creating recirculating motions and sometimes these phenomena tend to obscure the large scale motions responsible for carrying oil particles to much larger depths than the wave heights. This large scale motion is not easily recognized experimentally except for the fact it is also responsible for

the entrainment of organic particles which makes life exist to large depths.

One may use one's knowledge of turbulent flows in general to come up with an adequate analytic approach to the problem of describing the flow. First one observes that the ordinary linear approach to the wave mechanisms furnishes a flow field which exhibits recirculation but which has no mean motion in the direction parallel to the surface of the sea. The recirculating motion connected with the waves becomes insignificant at depths greater than a couple of wave heights. Closer examination of the fluid motion in the upper layer shows however that there is a mean horizontal velocity component "superimposed" on the wave motion, and this velocity component may vary with the horizontal distance. A simple consideration of the equation of continuity will then show that under such circumstances a vertical velocity component in the ocean is inevitable, and that it will penetrate to depths comparable to the distance over which the change in the horizontal velocity components take place. This may be an order of magnitude larger than the wave height.

There is no immediate and direct way of predicting this type of mean motion. One may however use the boundary layer flow which is described in Sec. 4.2.2 to exhibit a certain relevant case. Fig. 4.5 shows the upper layer of the ocean in which there is a horizontal current U_0 as shown by the velocity profile. (A two-dimensional situation is assumed.) At the surface (the waves have been neglected) a horizontal shear stress in the x-direction (opposite to U_0) is supposed to act due

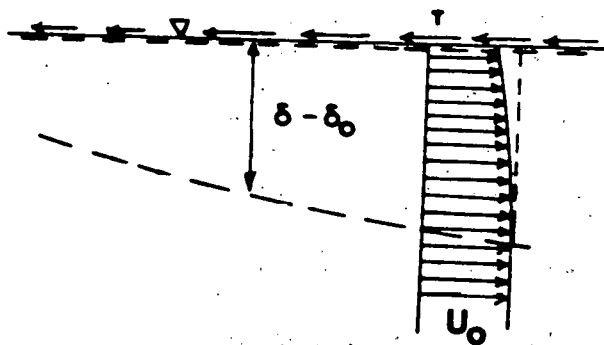


Fig. 4.5

to wind. If now this shear stress varies in the proper way, a boundary layer type of flow will develop in the upper layer and the situation is similar to that of Fig. 4.4. Thus the results of Sec. 4.2.2 are immediately applicable to the situation at hand and several cases of shear stress distribution on the surface have been considered whereby the following quantities have been computed as functions of the non-dimensional distance $(Re_x - Re_{x_0})$:

$\tau/\rho U_0^2$ = non-dimensional shear stress distribution

\bar{u}/U_0 = non-dimensional horizontal velocity component at the surface

\bar{v}/\bar{v}_0 = non-dimensional vertical velocity component at the surface

\bar{v}_∞/\bar{v}_0 = non-dimensional vertical velocity component at a depth equal to and/or greater than the boundary layer thickness $\delta - \delta_0$.

The computations are based on the equations of Sec. 4.2.2 and the computer programs used are exhibited in the Appendix. Fig. 4.6, 4.7, and 4.8 give the variation along the "surface" of the different quantities. The corresponding streamline pattern is exhibited in Fig. 4.9 where the dashed line represents the boundary of the region in which the expressions used are valid. It is seen how the streamlines indicate a vertical velocity (downwards) and the fate of oil droplets in this environment will be discussed in Section 4.3.

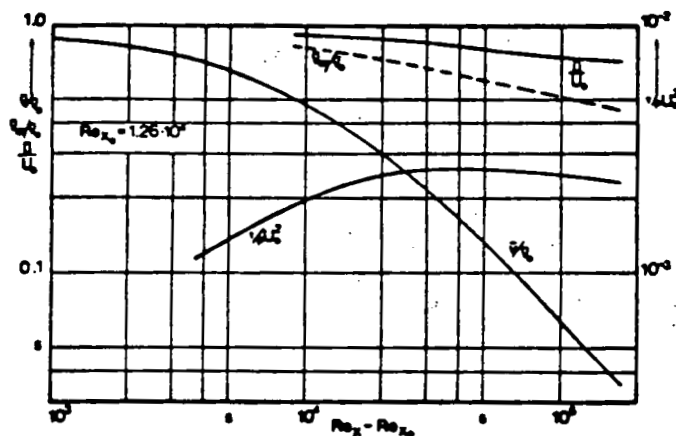


Fig. 4.6

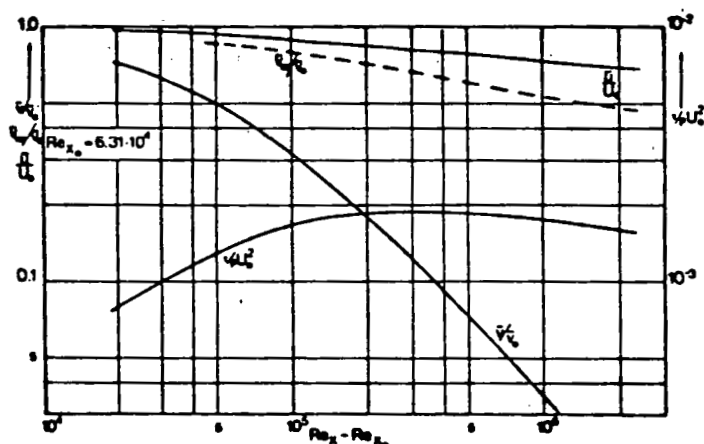


Fig. 4.7

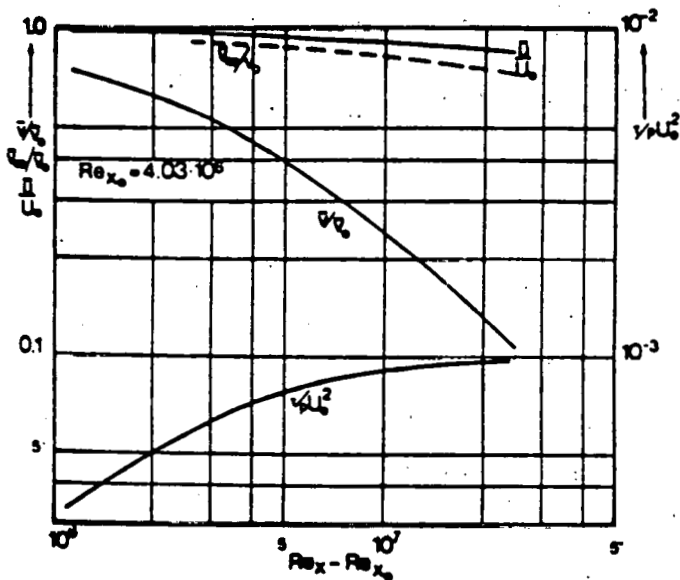


Fig. 4.8

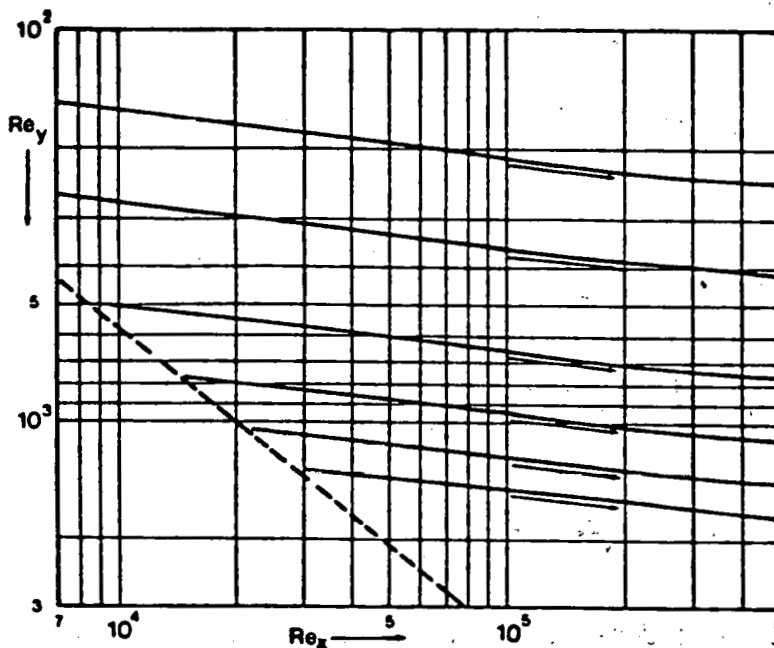


Fig. 4.9

4.2.4 The Jet Flow

It has been shown how the turbulent boundary layer can be used to model the downward flow in the ocean which in a certain case will occur and which is caused by the horizontal component of the mean velocity gradient. Since this only represents a special situation, one may try to find other models which will be useful in other situations. One such type of flow is the jet flow.

The jet flow is characterized by the fact that it is a self-similar type of turbulent flow. However, most of the jet investigations operate with a velocity field which corresponds to a non-vanishing velocity component at infinity normal to the jet-axis. The more proper velocity

field would be one exhibiting recirculation, and Persen-Skaug [7] have suggested just that type of velocity profile. The present investigation will start from this assumption and present the flow field as

$$\left. \begin{aligned} \frac{\bar{u}}{U_c} &= (\xi^2 + 1)^{-1/4} f(\eta) \\ \frac{\bar{v}}{U_c} &= \frac{1}{2} (\xi^2 + 1)^{-3/4} \xi \left\{ 2\eta f(\eta) - \int_0^\eta f(z) dz \right\} \end{aligned} \right\} (4.1)$$

where $f(\eta)$ is a non-specified velocity profile, η is the non-dimensional distance normal to the jet axis and ξ is the non-dimensional distance along the jet axis.

$$\left. \begin{aligned} \xi &= (x - x_0)/A \\ \eta &= \frac{y}{A} (\xi^2 + 1)^{-1/2} \end{aligned} \right\} (4.2)$$

Here A and x_0 are parameters important in the description of the jet flow but for the moment these are left for future consideration in the present context.

With this preliminary information one may now explore the jet flow somewhat closer. The velocity profile $f(\eta)$ is specified as

$$f(\eta) = e^{-\eta^2} - \frac{2B\eta^2}{\sqrt{\pi}(B^2 + \eta^2)} \quad (4.3)$$

where B is a constant to be determined later. It is observed that

$$\int_0^\eta f(z) dz = \int_0^\eta e^{-z^2} dz - \frac{2B}{\sqrt{\pi}} \int_0^\eta \frac{z^2}{(B^2 + z^2)} dz \quad (4.4)$$

which can be rewritten as:

$$\int_0^\eta f(z) dz = \frac{\sqrt{\pi}}{2} \operatorname{erf}(\eta) + \frac{\eta B}{\sqrt{\frac{2}{\pi}}(B^2 + \eta^2)^{-1}} - \frac{1}{\sqrt{\pi}} \operatorname{arc} \tan\left(\frac{\eta}{B}\right) \quad (4.5)$$

It is seen that

$$\lim_{\eta \rightarrow \infty} \int_0^{\eta} f(z) dz = 0$$

$$\lim_{\eta \rightarrow \infty} f(\eta) = 0$$

(4.6)

This means that the velocity field dies out (in view of (4.1)) as $\eta \rightarrow \infty$ (i.e. for large values of y).

The stream function Ψ for the flow under consideration will now be expressed as

$$\Psi = AU_c (1 + \xi^2)^{1/4} \int_0^{\eta} f(z) dz \quad (4.7)$$

4.2.5 The Analogous Flow in the Ocean

Just as the boundary layer flow exhibited in Section 4.2.2 was shown to have a bearing on the flow in the upper layer of the ocean, the jet flow may also be shown to be applicable. If one imagines the scenario when a wind has produced a mean horizontal velocity in the upper layer of the ocean and then ceases to blow, the situation will be as shown in Fig. 4.10 where the velocity profile is similar to that of the jet with a zero velocity gradient at the surface indicating the absence of a shear stress at the surface. The horizontal velocity will eventually die down and a

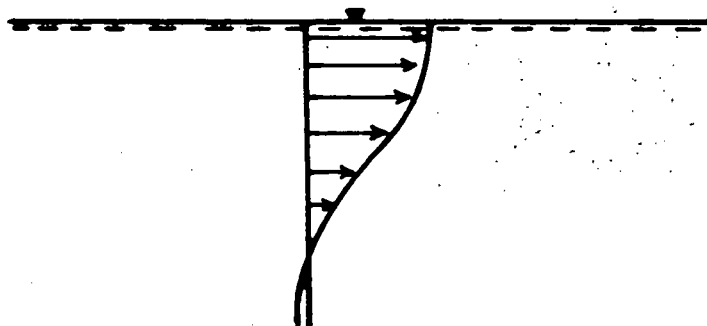


Fig. 4.10

velocity gradient in the horizontal direction will produce a downward flow in the ocean. Thus the jet flow has found its analogue in the large scale flow structure in the ocean. The flow is illustrated in Figs. 4.11 and 4.12. It is seen that the flow patterns are very similar even though the parameter is $B = 2$ and $B = 5$ respectively. Consequently, only one case will be treated subsequently when the fate of oil droplets in this type of flow is considered in Section 4.3.

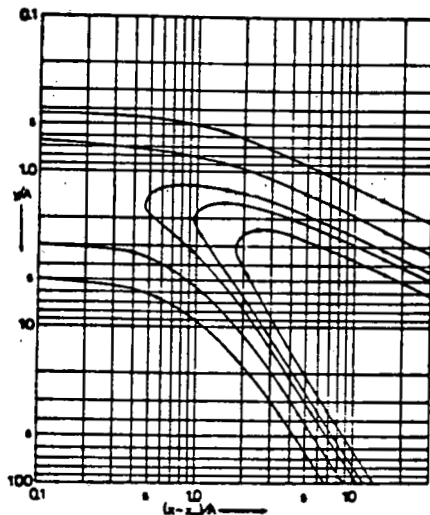


Fig. 4.11 Streamlines in the recirculating flow, $B = 2$

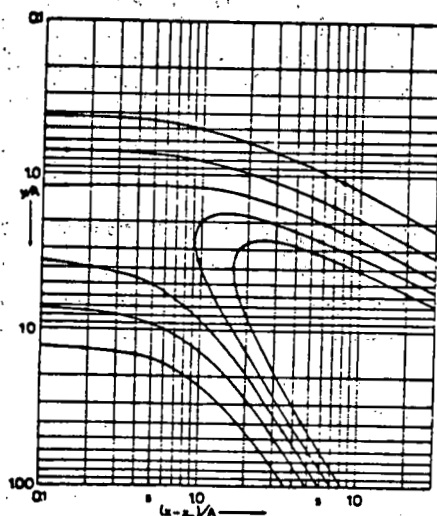
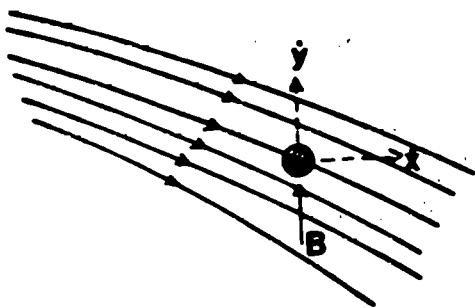


Fig. 4.12 Streamlines in the recirculating flow, $B = 5$

4.3 THE PATHS OF OIL DROPLETS IN THE OCEAN

4.3.1 Introduction

It has been shown that the entrainment of oil in the water column is governed by the recirculating motion which can be found in the ocean due to the nonuniform velocity distribution of the horizontal velocity component in its upper layer. It is the purpose of this paper to explore the possibility of studying this process more in detail.

4.3.2 The Equations of Motion

It will be assumed that the motion of an oil droplet can be described on the basic assumption that its motion does not affect the flow field. One will then have the flow field described through the velocity components $u(x,y)$ and $v(x,y)$ which may be considered as given or known functions. The position of an oil droplet will be, x,y , its velocity \dot{x},\dot{y} and its acceleration \ddot{x},\ddot{y} . Its mass is m .

Fig. 4.13 Oil Droplet in a Flow field

The set of equations of motion will now be:

$$F_x = m\ddot{x}$$

$$F_y + B = m\ddot{y}$$

(2.1)

where B is the buoyancy force, and F_x and F_y are the forces exerted on the droplet by the fluid. The latter forces will depend on the relative velocity between the droplet and the fluid. The drag force on a sphere (droplet) is given as a function of the Reynolds number

$$Re = \frac{VD}{\nu}$$

(2.2)

where V is the relative velocity of the sphere to the fluid
 D is the diameter of the sphere

ν is the kinematic viscosity of the fluid

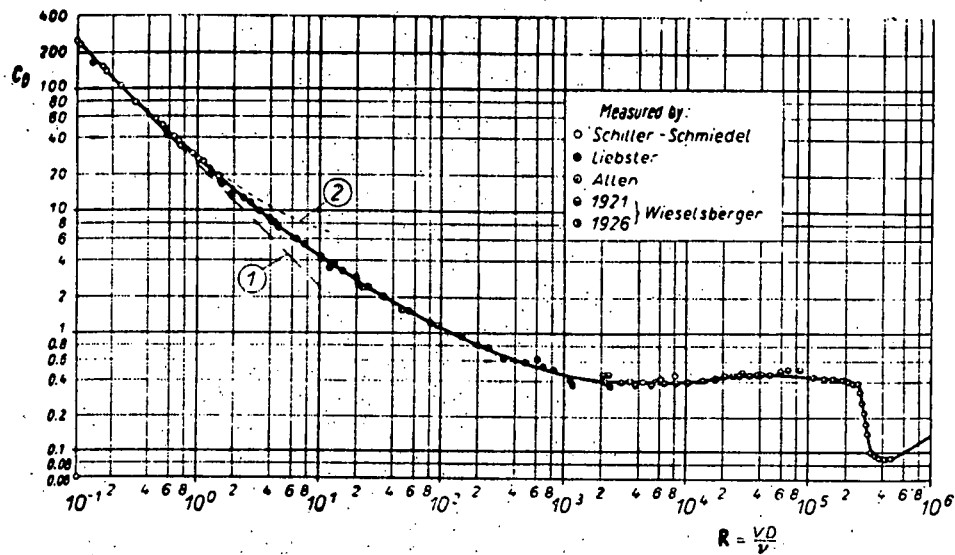


Fig. 1.5. Drag coefficient for spheres as a function of the Reynolds number
Curve (1): Stokes's theory, eqn. (6.10); curve (2): Oseen's theory, eqn. (6.13)

Fig. 4.14

The drag force on a sphere in a cross flow is given in Fig. 4.14 which is a reproduction of Fig. 1.5 in H. Schlichting [8], where c_d is defined as the drag force F normalized with the stagnation pressure $\frac{1}{2}\rho V^2 A$, A , being the central cross section of the sphere. The drag force is seen to be proportional to the velocity for very small Re-numbers and proportional to the square of the velocity in the range $10^4 < Re < 10^5$. The most likely situation for small oil droplets seems to be in the lower range of Re-numbers, and consequently the components of the drag force will be:

$$\left. \begin{aligned} F_x &= -k[\dot{x} - u(x,y)] \\ F_y &= -k[\dot{y} - v(x,y)] \end{aligned} \right\} (2.3)$$

where k is a proportionality factor. Introduced into (2.1) this will give

$$\boxed{\begin{aligned} m\ddot{x} + k\dot{x} &= ku(x,y) \\ m\ddot{y} + k\dot{y} &= kv(x,y) - B \end{aligned}} \quad (2.4)$$

which are the basic equations governing the motion of the oil droplet.

One may now assume that the flow field exhibits a characteristic length A and a characteristic velocity U_0 by means of which the following non-dimensional quantities can be introduced:

$$\begin{array}{l}
 \xi = (x - x_0) / A \quad = \text{non-dimensional x-coordinate} \\
 \zeta = y/A \quad = \text{non-dimensional y-coordinate} \\
 \tau = t \frac{U_c}{A} \quad = \text{non-dimensional time} \\
 \left. \begin{array}{l} u^* = u/U_c \\ v^* = v/U_c \end{array} \right\} = \text{non-dimensional velocity components}
 \end{array} \quad (2.5)$$

With these quantities the basic equations will appear in the form:

$$\begin{array}{l}
 \frac{d^2 \xi}{d\tau^2} + \lambda \frac{d\xi}{d\tau} = \lambda u^*(\xi, \zeta) \\
 \frac{d^2 \zeta}{d\tau^2} + \lambda \frac{d\zeta}{d\tau} = \lambda v^*(\xi, \zeta) - \beta
 \end{array} \quad (2.6)$$

where

$$\begin{array}{l}
 \lambda = \frac{kA}{mU_c} \\
 \beta = \frac{B \cdot A}{mU_c^2}
 \end{array} \quad (2.7)$$

The physical quantities in these dimensionless parameters are:

$$\begin{array}{l}
 U_c = \text{the characteristic velocity of the flow field} \\
 m = \rho_0 V = \text{mass of the droplet} \\
 V = \frac{\pi d^3}{6} \quad \text{volume of the droplet} \\
 d = \text{diameter of the droplet} \\
 A = \text{characteristic length of the flow field} \\
 B = g(\rho - \rho_0)V = \text{buoyancy force of the droplet} \\
 k = \text{proportionality factor for the drag force} \\
 \quad \text{which is here assumed proportional to the} \\
 \quad \text{velocity}
 \end{array} \quad (2.8)$$

From Fig. 4.2 one finds the drag force F under such conditions as

$$F = 25 \cdot \frac{1}{2} v^2 \rho \frac{1}{4} \pi d^2 \left(\frac{vd}{v} \right)^{-1} \quad (2.9)$$

$$= 9.81 \cdot v \mu d \quad \text{i.e. } k = 9.81 \cdot \mu \cdot d$$

One may now reformulate the two parameters in (2.7) as follows:

$$\lambda = \frac{9.81 \cdot \mu \cdot d \cdot A}{\rho_o \frac{\pi}{6} d^3 U_c} = 18.74 \frac{\rho}{\rho_o} \frac{v}{U_c} \frac{A}{d} \quad (2.10)$$

$$\beta = \frac{(\rho - \rho_o) g \frac{\pi}{6} d^3 \cdot A}{\rho_o \frac{\pi}{6} d^3 U_c^2} = \left(\frac{\rho}{\rho_o} - 1 \right) \frac{gA}{U_c^2} \quad (2.11)$$

The dimensional quantities will here have the following numerical values.

$$\begin{aligned} \rho &= \text{density of water (or sea water)} && 1.0 \text{ [gr/cm}^3\text{]} \\ \rho_o &= \text{density of oil} && 0.86 \text{ [gr/cm}^3\text{]} \\ v &= \text{viscosity of water} = 1.0 \cdot 10^{-6} \text{ [m}^2\text{/s]} \\ A &= \text{length characterizing the flow field} && (2.12) \\ &&& 1 \text{ [m]} < A < 10 \text{ [m]} \\ U_c &= \text{velocity characterizing the flow field} \\ &&& 1 \text{ [m/s]} < U_c < 5 \text{ [m/s]} \\ d &= \text{diameter of a droplet} && 10^{-6} \text{ [m]} < d < 10^{-4} \text{ [m]} \end{aligned}$$

A Reynolds number for the problem may now be formed as

$$Re = \frac{U_c d}{v} \quad (2.13)$$

and with the numerical values given above the following range of variation of Re is obtained:

$$1 < Re < 500 \quad (2.14)$$

Furthermore, the two parameters λ and β will have a range of variation like:

$$\left. \begin{aligned} 4.36 \cdot 10^2 < \lambda < 2.18 \cdot 10^3 \\ 0.064 < \beta < 16 \end{aligned} \right\} (2.15)$$

It is now from the magnitude of the parameter λ rather obvious that cases may occur where the acceleration terms in (2.6) become negligible, and consequently the equations reduce to:

$$\left. \begin{aligned} \frac{d\xi}{d\tau} &= u^*(\xi, \zeta) \\ \frac{d\zeta}{d\tau} &= v^*(\xi, \zeta) - \beta/\lambda \end{aligned} \right\} (2.16)$$

This may be carried even further by observing that the flow field is two-dimensional and that in the case of an incompressible fluid, one then has a stream-function Ψ for the flow from which the velocity components are deduced:

$$\left. \begin{aligned} u^* &= \frac{\partial \bar{\Psi}}{\partial y} / U_c \\ v^* &= \frac{\partial \bar{\Psi}}{\partial x} / U_c \end{aligned} \right\} (2.17)$$

Introducing the two non-dimensional quantities ξ and ζ from (2.5) one may rewrite this

$$\left. \begin{aligned} u^* &= \frac{\partial \Psi}{\partial \zeta} / AU_c \\ v^* &= - \frac{\partial \Psi}{\partial \xi} / AU_c \end{aligned} \right\} (2.18)$$

which may be introduced into (2.16) to give:

$$\left. \begin{aligned} \frac{d\xi}{d\tau} &= \frac{\partial \Psi}{\partial \zeta} / AU_c \\ \frac{d\zeta}{d\tau} &= \frac{\partial \Psi}{\partial \xi} / AU_c - \beta/\lambda \end{aligned} \right\} (2.19)$$

The ratio of these equations may be written

$$\frac{d\zeta}{d\xi} = \frac{-\frac{\partial \Psi^*}{\partial \xi} - \beta/\lambda}{\frac{\partial \Psi^*}{\partial \zeta}} \quad (2.20)$$

which is the differential equation for the path of the droplet given by ζ as a function of ξ and where Ψ^* is defined as

$$\Psi^* = \Psi/U_c A \quad (2.21)$$

The solution to (2.20) is easily found by introduction of the path-function θ :

$$\theta = \Psi^* + \xi\beta/\lambda \quad (2.22)$$

Equation (2.20) now reduces to

$$\frac{d\zeta}{d\xi} = -\frac{\partial \theta / \partial \xi}{\partial \theta / \partial \zeta} \quad (2.23)$$

with the solution

$$\theta = \text{constant.} \quad (2.24)$$

Under the given conditions, the path of an oil droplet is given in terms of the streamfunction of the flow as

$$\Psi^*(\xi, \zeta) + \xi\beta/\lambda = \text{const.} \quad (2.25)$$

This general solution will now be examined in the two cases of recirculating flow treated earlier.

4.3.3 Particle Paths in a Boundary Layer Type Flow

In the discussion of the recirculating flow in the ocean (Section 4.2) the boundary layer type flow was treated and the analytic description of the flow was carried so far that expressions for the streamlines in the flow were established. Since the path of oil particles (droplets) of the size of interest here is given in terms of the streamfunction of

the flow (2.25), the program STREAM (Appendix) has been used to plot the particle paths in environments given as the flow of Fig. 4.9. The result of such computations is shown in Fig. 4.15. As seen from (2.25) the results will depend on the Particle-number $P = \beta/\lambda$.

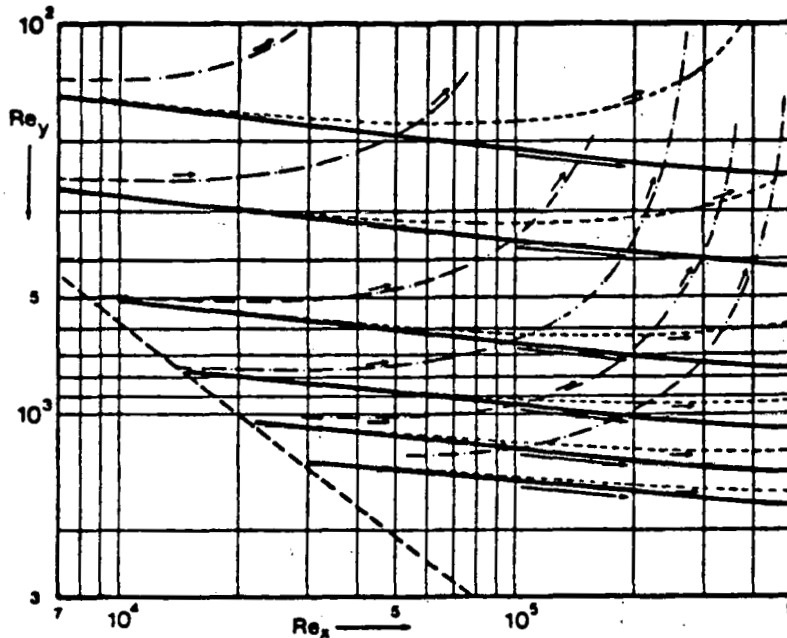


Fig. 4.15 Paths of Oil Particles in a Boundary layer type flow
 $P = 0.001$
 - - - - - $P = 0.0001$

This P-number can be expressed through (2.10) and (2.11) as

$$P = \frac{(\rho - \rho_0)gV}{kU_c} = \frac{\text{buoyancy force}}{\text{characteristic drag force}} \quad (3.1)$$

or as

$$P = 0.0534 \left(1 - \frac{\rho_0}{\rho}\right) \frac{gd^2}{\nu U_c} \quad (3.2)$$

It is easily seen that the P-number decreases with decreasing droplet size and increasing characteristic velocity of the flow. The P-number for the particles in question will be very small and for this reason Fig. 4.15 has been prepared with $P = 0.001$ and $P = 0.0001$. In the first case, the oil particles are seen to rise relatively rapidly, i.e., they have

remark may be made. From Fig. 4.16 one may pick out the non-dimensional depth d to which an oil particle will be carried if it initially is placed at a depth d_i .

d_i/A	$P = 0.01$		$P = 0.001$	
	d/A	d/d_i	d/A	d/d_i
0.43	1.00	2.33	3.30	7.67
0.70	1.85	2.64	5.60	8.00
1.20	3.30	2.75	10.00	8.33

This shows that a particle can, depending on its P-number, be carried to depths many times the original depth to which it is being brought by actions at the surface.

4.4 THE EXPERIMENTS

4.4.1 Introduction

Three different experiments pertaining to the entrainment process are described in Section 4.1. The Wind-Wave experiment was conducted by Steven Parks under the supervision of Dr. R. Dowdell and a description of this activity is found in Section 3 of this report.

The Drop-Size Experiment was conducted by Mathew Cherian and the results obtained in his 20 gallon tank will be given here and commented upon.

The Rain-Drop Experiment was conducted by Ted Kawazoe and both experiments were supervised by the author. The earlier experimentation in the rain drop apparatus was supervised by Dr. Cornillon.

4.4.2 The Parameters

Conditions under which the experiments are conducted are determined by several parameters whose importance may not be initially recognized. One may easily identify such parameters as surface tension, temperature, oil slick thickness, intensity of the recirculating flow, etc. as important ones, but it is difficult offhand to judge their relative influence. One or more may be of such importance that it obscures the influence of others. The experimentation was originally planned exclusively in sea water but practical considerations led to some experiments being performed in fresh water. The influence of the type of water on the entrainment could thus be commented on.

Because of difficulties in keeping a constant quality of the sea water to be used, it was decided to measure the surface tension of the water/air interface. In this way one hoped to be able to detect natural surfactants that might be present in the water. For that purpose, a test

was made to see how sensitive such a measurement would be to the presence of the dispersant COREXIT 9527 in the water. The result of this test is shown in Fig. 4.17. It is seen that very small concentrations give very large effects and that the surface tension water/air for a concentration of 2.5[mg/l] is almost as small as for COREXIT 9527 alone.

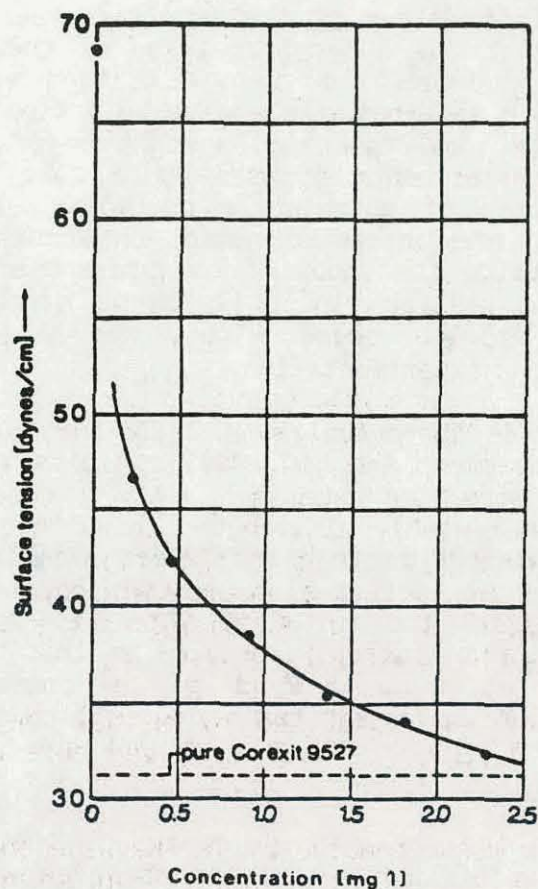


Fig. 4.17 The Effect of Addition of a Dispersant on Measured Surface Tension Water/Air

During this experiment it was discovered that the actual result of a measurement was dependent on the person who performed the test, i.e., that an element of personal judgment was involved. The values should therefore only be given a relative importance.

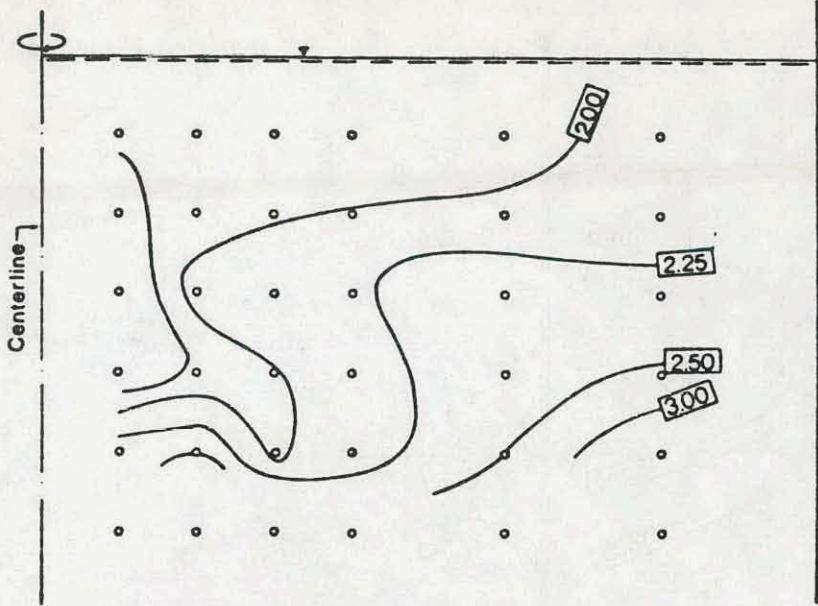
The next step in the investigation of the parameters was to find a way to ascertain the "strength" of the recirculating flow which presumably is responsible for the entrainment. For that purpose, a hot film Anemometer DISA with a probe 55A87 (conical, quartz coated) was used.

Its performance was examined in a towing tank for calibration and subsequently used for examining the flow created in the tanks by the impellers.

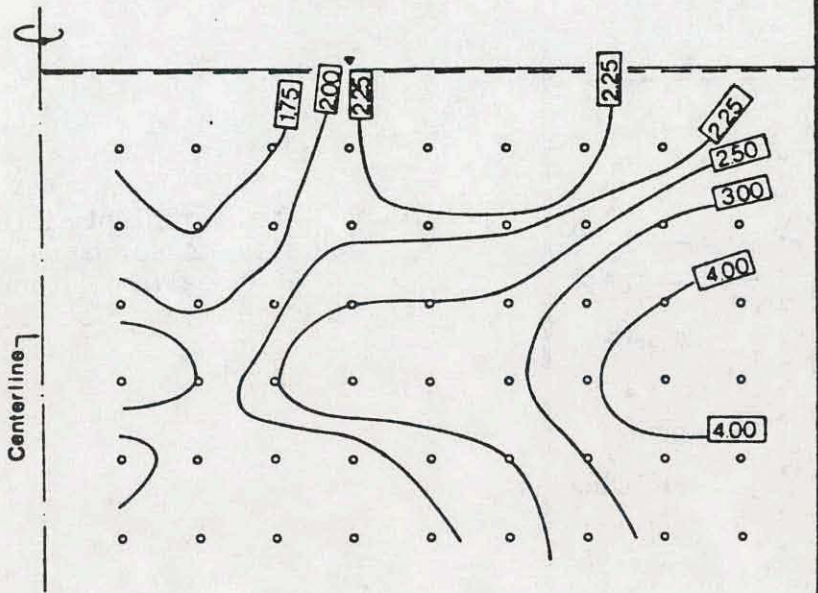
The results of the flow measurements in the 20 gallon tank of the Drop-Size-experiment are shown in Fig. 4.18 where a plot of a plane through the centerline of the tank is shown with the measuring stations indicated by small circles and with curves of equal mean velocity. The plots are shown for different values of the impeller speed (measured in rpm) and it is observed that the general features of the flow pattern seem to be preserved with an increase in mean velocities as the impeller speed is increased. It is clear that a closer examination of the velocity field in the immediate subsurface region might be of interest when exploring the details of entrainment in cases where the flow itself is responsible for the creation of entrainable particles. Such a study must, however, in light of the increased demand on accuracy, equipment and time be considered outside the scope of the present effort. It is, however, observed that the radial velocity gradient along the surface increases with increasing impeller speed. Thus, the impeller speed may be used as a parameter in the experimentation.

The recirculating flow is characterized also by the turbulent intensity. This quantity was measured and Fig. 4.19 exhibits the results in the 20 gallon tank of the Drop-Size experiment. It is observed that the turbulent intensity is rather evenly distributed throughout the tank. A feature which may be of interest is that the lowest impeller speed seems to create a greater turbulent intensity close to the impeller than do the higher speeds. In all cases, the turbulent intensity is of the same order of magnitude. Thus one may already conclude at this point that any influence on the entrainment process, which may be observed due to a change in impeller speed, may be attributed to a corresponding change in velocity gradient along the surface and not necessarily to a change in turbulent intensity.

These remarks conclude the preliminary remarks on the parameters of the experiments. The effect of each one of the other parameters will be discussed in the presentation of the results.



RPM: 125



RPM: 150.8

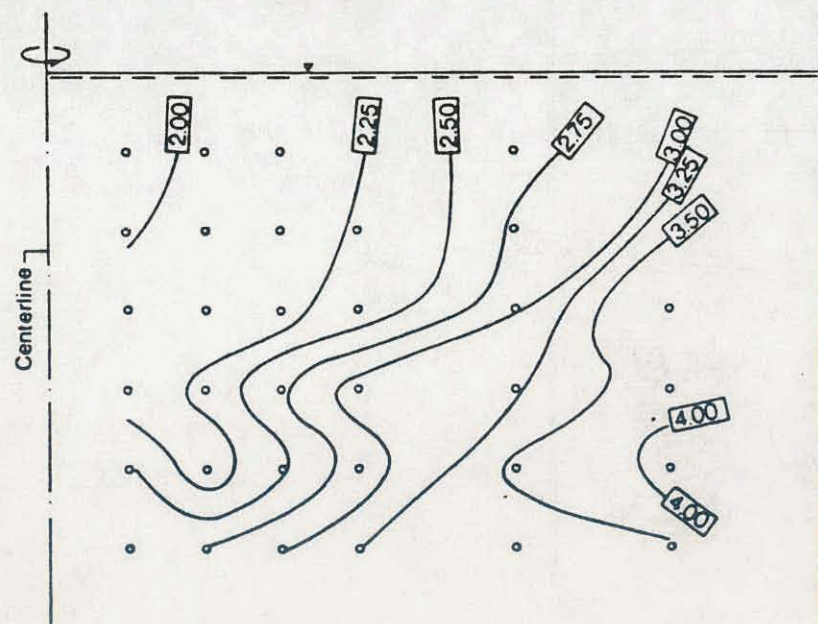
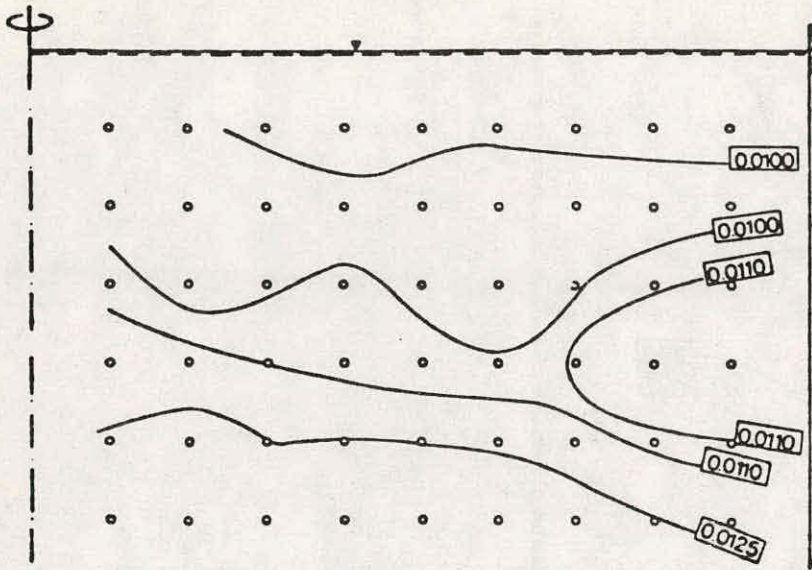
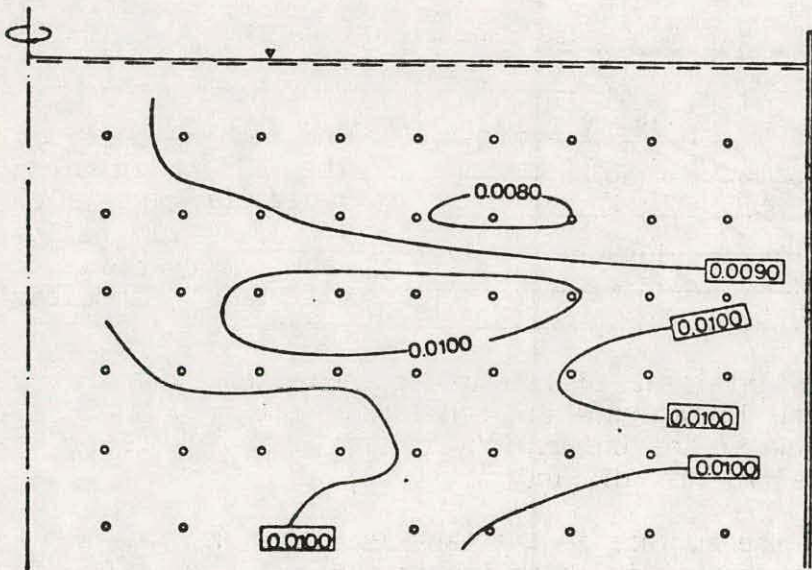


Fig.4.18 The mean velocity of the turbulent recirculating flow in the 20 gallon tank measured at different impeller speeds.

98.7 rpm



125 rpm



150 rpm

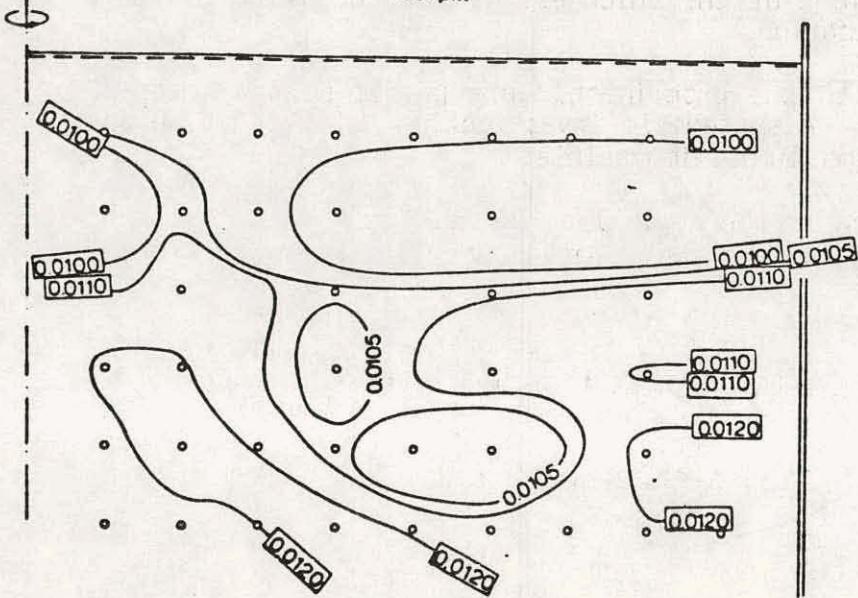


Fig.4.19 The turbulent intensity measured in the 20 gallon tank's upper part at different impeller speeds.

4.4.3 The Drop Size Experiment

In the exposition of the author's concept of the entrainment process, a mechanical agitation of some sort, acting at the surface was supposed to be responsible for the creation of "entrainable particles". In the Rain Drop Experiment (Section 4.4.4), the rain impinging on the oil slick is such a mechanical agitation. As pointed out in Section 4.1, some focus their attention on the breaking waves as the mechanism for introducing the necessary action. In the present experimentation no mechanical agitation other than what is being brought about by the recirculating flow (impeller) is present at the surface. It is important to show that entrainment can be brought about even in the absence of breaking waves.

Table 4.1 shows the values of the different parameters used in the different experiments. It is noticed that the surface tension data

Table 4.1 Experimental Parameters of Drop-Size Experiments

	10/17	10/29	11/16	12/07	12/19	02/02	02/21	03/08
WATER:	FRESH	FRESH	SEA	SEA	SEA	FRESH	FRESH	SEA
TEMPERATURE:	21.5°-22°C	25°C	20°-16°C	17°-14°C	7°-4°C	17°-14°C	19°-14.5°C	-
OIL ADDED:	42.8	44.8	41.6	97.0	95.4	50.2	47.3	48.2
SURFACE TENSION:	68.1	68.3	69.4	69.2	69.9	69.1	68.8	69.4
IMPELLER SPEED:	65.8	149.6	155.9	150.6	148.7	310	153.5	230

indicate what may seem an insignificant difference between fresh water and sea water. The data in the latter case are consistently higher, but with a difference which in view of the uncertainty of the measurements, makes a distinction between the two very difficult.

The amount of oil added to the surface in the tank is either approximately 30 ml or 60ml. This is the way in which the thickness of the oil is varied. A finer gradation of the thickness is not necessary in view of the scope of the investigation.

The temperature at which the experiments were performed was imposed by the ambient temperature. A systematic investigation of the influence of this parameter thus became almost impossible.

Fig. 4.20 shows a sketch of the so-called "20 gal. tank". It is seen to be equipped with 4 taps at different depths under the surface through which samples of the water with the entrained oil can be taken. The impeller was placed very close to the bottom of the tank and the measurements of Figs. 4.18 and 4.19 were made in the region above a depth of 10", i.e. well above the impeller. The entrainment was measured as concentrations of oil in the samples taken through the taps according to a determined time schedule. This schedule ran first for 4 hours and was later changed to 10 hours; in both cases control samples were taken after

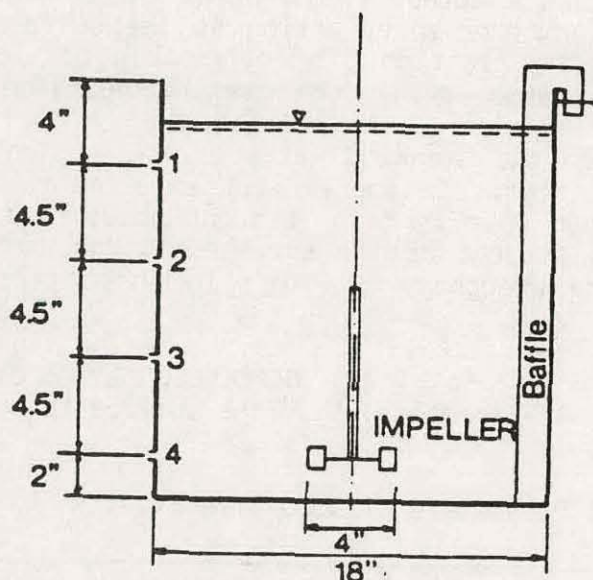


Fig. 4.20 The "20 gal. tank" of the Drop-Size-Experiment

24 hours. The results of these measurements are exhibited in Figs. 4.21a - d. The running time for the impeller is shown in the diagrams.

In contemplating the conclusions which may be drawn from these results the scarcity of them, and consequently their inherent uncertainty, should not be overlooked. However, some results seem well established and will also be supported from other sources.

Starting with Fig. 4.21b, one observes that the three experiments have been made under almost identical conditions as far as water type, impeller speed and surface tension is concerned. In E 12/07 and E 12/19 even the same amount of oil was added. The temperature during the experiments differs however by approximately 10 C without any noticeable difference in entrainment. Thus it seems that the temperature is not a parameter which in this range strongly influences the entrainment. If however the third experiment E 11/16 is considered, a comparatively large increase in entrainment is noticed and since temperature is ruled out, this can only be attributed to the fact that in the latter case the oil film is thinner (only half as much oil added). So, with the slim background of three experiments (E 11/16, E 12/07, E 12/19) the following conclusions are attempted:

1. Within the range of variation of the temperature (4° - 14° C) the influence of temperature on entrainment seems negligible.
2. The entrainment from a thin slick is, under the same conditions, larger than from a thick slick.

These preliminary conclusions will be examined in the light of later results.

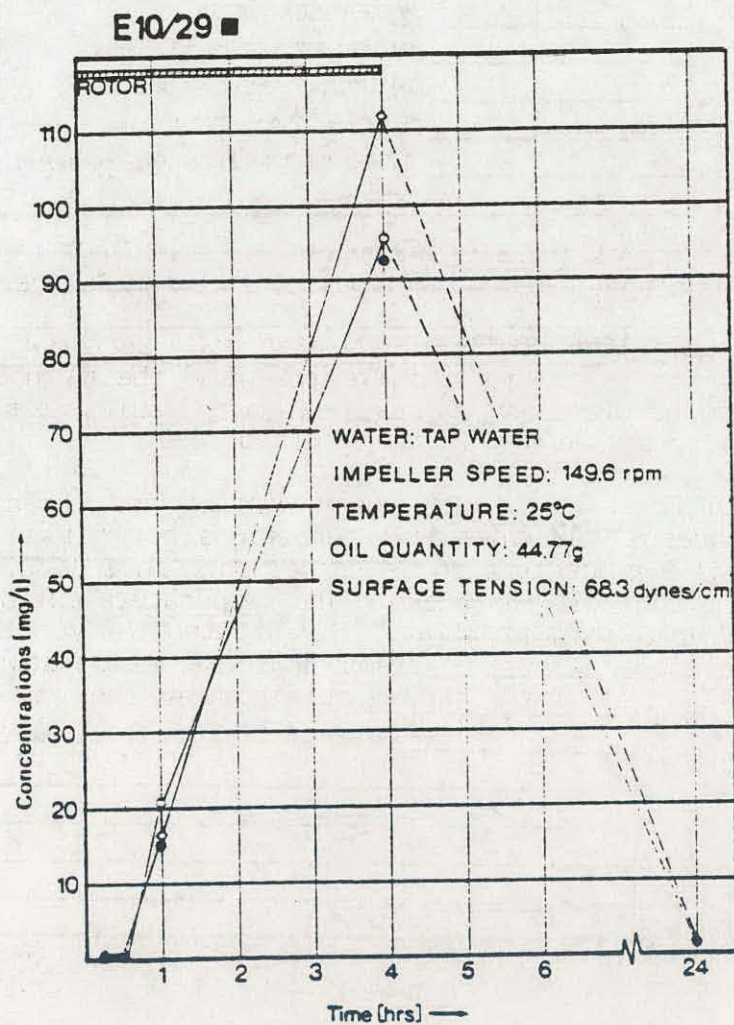
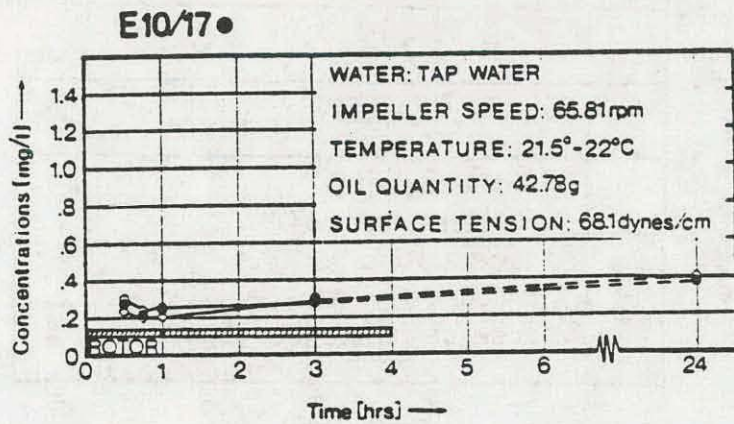


Fig. 4.21a

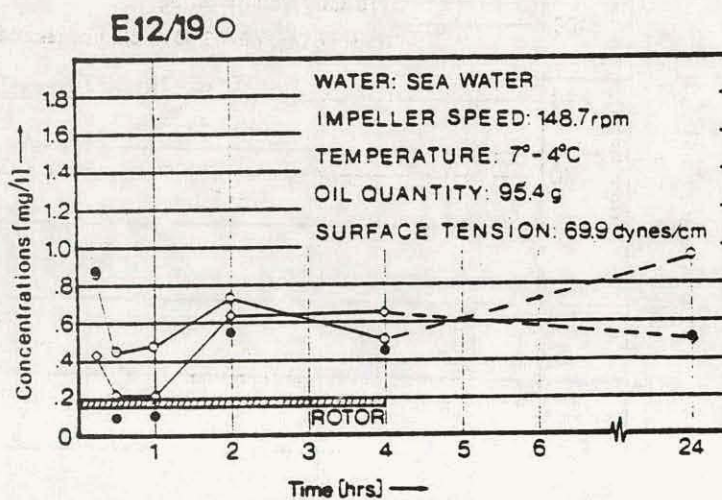
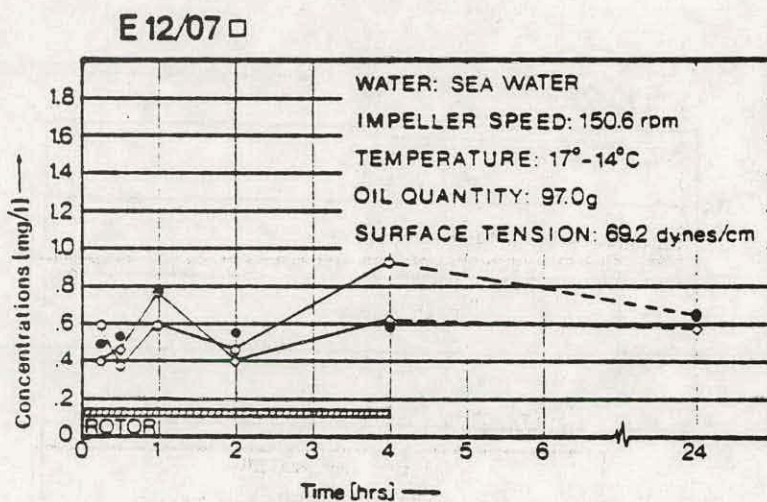
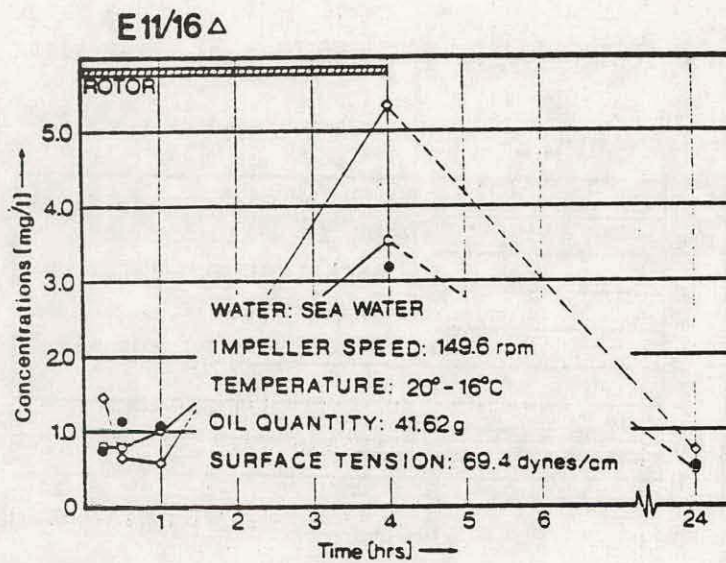
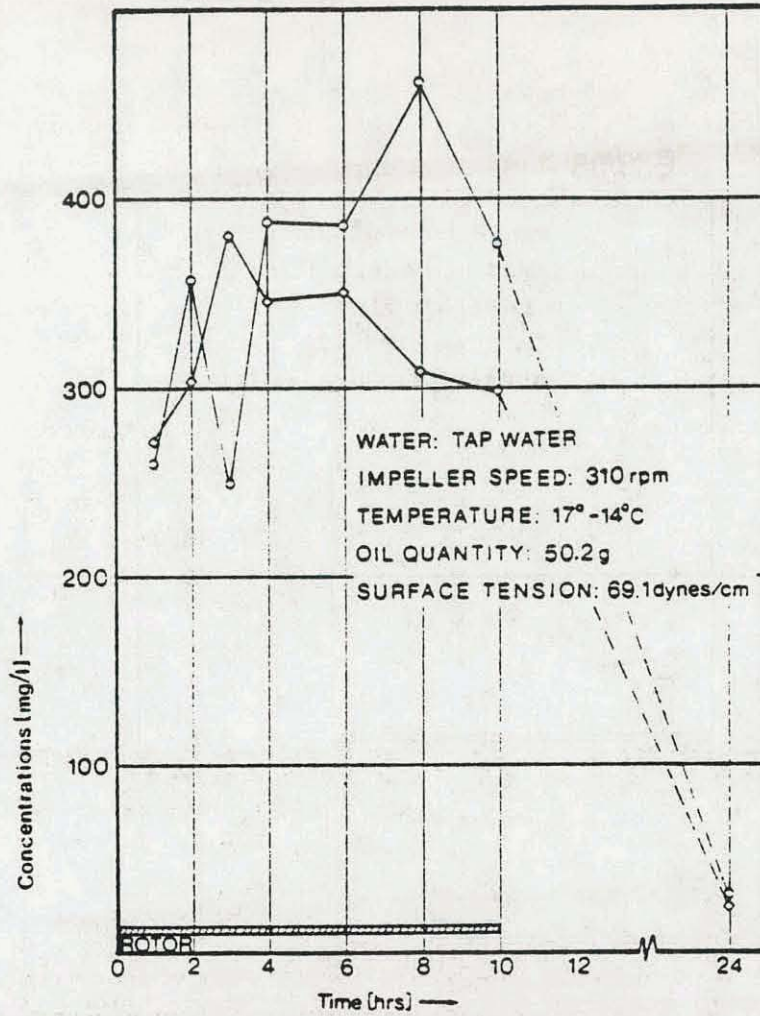


Fig. 4.21b

E 02/02 ◆

4-37



E 02/21 ▲

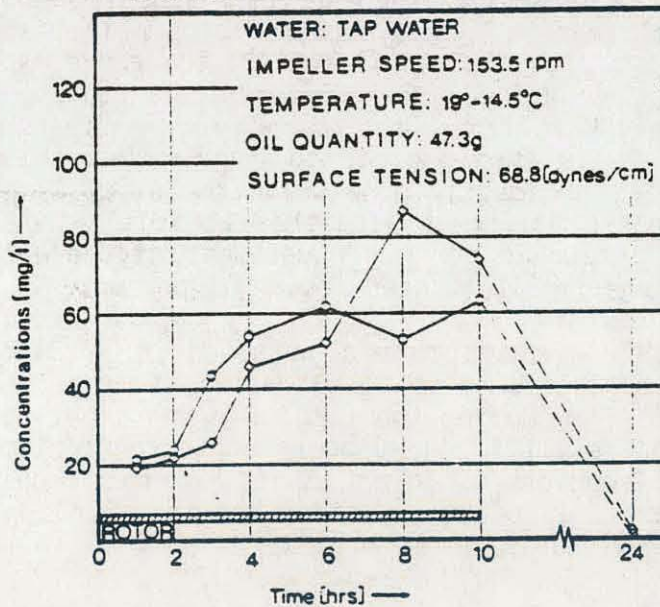


Fig. 4.21c

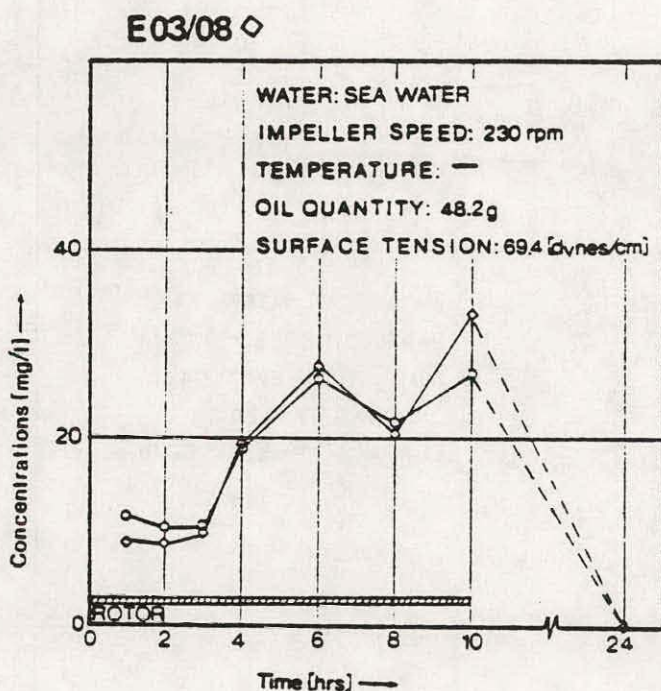


Fig. 4.2ld

At this point it might be mentioned that the impeller speed was adjusted in such a way that small vortices could be identified as "dents" in the water surface, which moved around, appeared and vanished in an apparent stochastic manner. This occurred at impeller speeds of approximately 150 rpm, i.e., at the speed used in the above experiments. It is thought that the occurrence of such vortices represent the mechanism whereby the oil slick is fragmented and whereby entrainable particles are being produced. It is then logical to deduce that this "fragmentation" due to vortices is more easily done where the slick is thin than when it is thick (in complete agreement with the result). Since it is desirable to establish the influence on the entrainment of the recirculating flow, the variation of the impeller speed becomes important.

If one considers the entrainment obtained in E 12/07 and E 12/19 one will find that very little is being entrained, in fact so little that the concentrations obtained during the time when the impeller is rotating are equivalent to those still found 20 hours after the recirculating flow was "stopped." This suggests a lower limit for the impeller speed below which very little oil is being entrained and this limit may depend on the oil slick thickness. This point will be reexamined in the light of subsequent results.

Consider now the results of Fig. 4.2la. A comparison between E 10/29

and E 11/16 shows that the values of temperature, oil slick thickness, impeller speed and surface tension are almost equal. Thus the tremendous difference in entrainment in the two cases may be attributed to the fact that one experiment is done in fresh water and the other in sea water. On the other hand, the experiment E 10/17, which is done under almost identical conditions except for the impeller speed being much less, show almost no entrainment. One is now faced with the following possible conclusions:

3. The entrainment of oil in the water column under otherwise equal conditions seems to occur much more easily in fresh water than in sea water. This is in contrast to other observations (see Section 4.4.5 Final Remarks)
4. Entrainment of oil in the water column is very strongly dependent on the "strength" of the recirculating flow.

The results at this point show that the samples from the different taps are influenced so much by occasionally trapped larger oil droplets that a concentration gradient in the vertical direction may not be experimentally determined. Thus the conclusions so far have been drawn on the basis of mean values of the instantaneous concentrations measured at the 3 taps.

It has furthermore been assumed that after 4 hours some kind of equilibrium state has been reached. This is tested in the experiments shown in Fig. 4.21c-d. where the period over which samples were taken is increased. It seems to be confirmed that the "equilibrium" has been reached after 4-6 hours.

The experiment E 02/21 is seen to be almost identical to E 10/29 as far as most parameters are concerned. There is however a difference in temperature between the two cases of approximately 10 C. This means that the previous statement about the influence of temperature perhaps must be modified, because there is a difference of 10 - 15% in concentration between the two cases which can be explained as the influence of temperature. The rather high concentration measured seems, however, to be a consistent result. The result of E 02/02 are obtained with a rather high value of the impeller speed. During the experiment it seemed as if all oil on the surface was being entrained. If one assumes from the data a uniform concentration of 350 [mg/l] in the water, the totally entrained mass of oil will be 26.5 [gr] or approximately half the oil added. Apparently this high value of the impeller speed represents the upper limit for sensible experimentation in the apparatus used.

Fig. 4.21d shows the results for a rather high value of the impeller speed and with sea water. Gathering all results, one may now present them as done in Fig. 4.22 where the mean maximum concentration is plotted as a function of the impeller speed. The legend used to identify the experiments are shown in Figs. 4.21 a-d.

It seems as if the following conclusions may be drawn:

1. The influence of temperature on the entrainment may hardly be estimated from the results of these experiments. Emphasis is

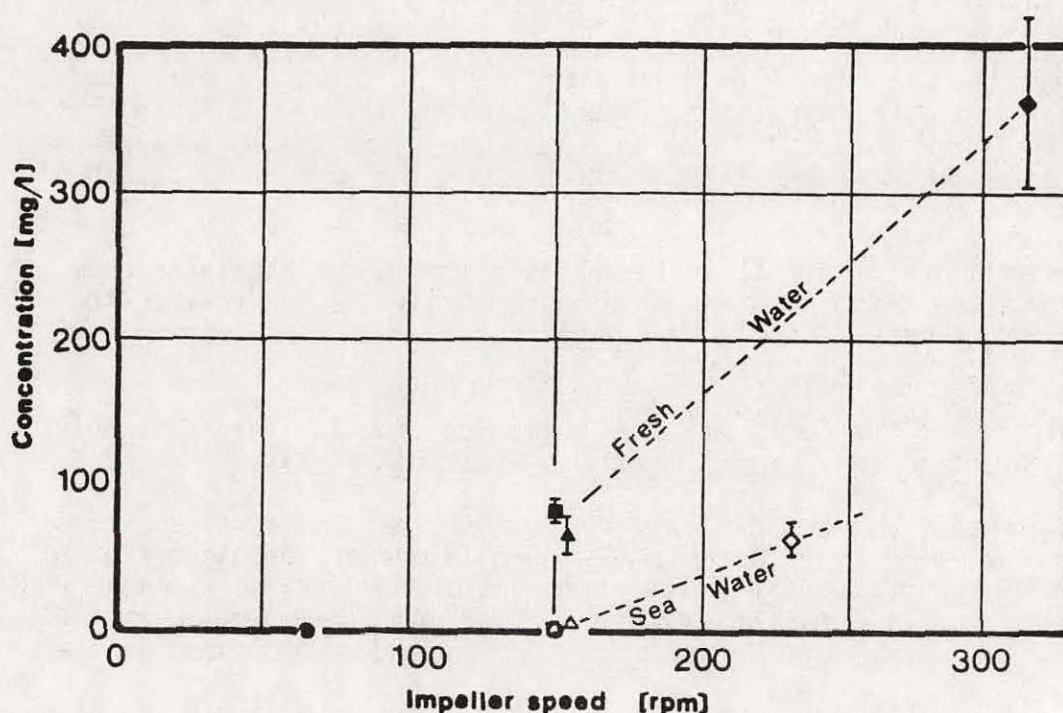


Fig. 4.22. Entrainment as a function of the "strength" of the recirculating flow (i.e. the impeller speed)

put on the scarcity of experimental evidence and the limited temperature range. (See the Rain-Drop experiment, section 4.4.4).

2. The entrainment from a thin slick is under the same conditions, larger than from a thick slick. (As before).
3. The entrainment of oil in the water column under otherwise equal conditions seems to occur much more easily in fresh water than in sea water. (As before, with reservations).
4. Entrainment of oil in the water column is very strongly dependent on the "strength" of the recirculating flow. (As before).

4.4.4. The Raindrop Experiment

This experiment is discussed in Section 4.1.5. It distinguishes itself from the experiment originally carried out in the same rig by the fact that an impeller has been installed at the bottom of the receiving tank. This creates a recirculating flow which, in the author's concept, is responsible for the entrainment. This experiment also distinguishes itself from the previous one (preceding section) in the presence of a mechanical agitation (rain falling) at the surface.

The parameters of the experiment are the same as in the preceding section but now one has the rain intensity as an additional parameter. The rain maker (tank B, Fig. 4.2) had a variable performance due to the clogging up of the needles producing the raindrops. This is due to the fact that salt water (sea) was used to produce the rain to avoid the complication of having a mixture of salt and fresh water at the surface. The rain intensity was attempted to be kept constant during the conduction of an experiment, but variations of 10% had to be accepted. The rain intensity may be expressed in different ways. One may give it as the amount of rain falling over the entire surface per unit time [l/hour]. One may however give it as the kinetic energy of the raindrops as they hit the surface. In this latter case, the rain intensity may be the same for different heights and different drop sizes as well as for different drop frequencies. An examination of this effect has so far not been made, and for the present purpose the first way of describing the rain intensity has been used.

Fig. 4.23 shows a sketch of the receiving tank. Water samples are

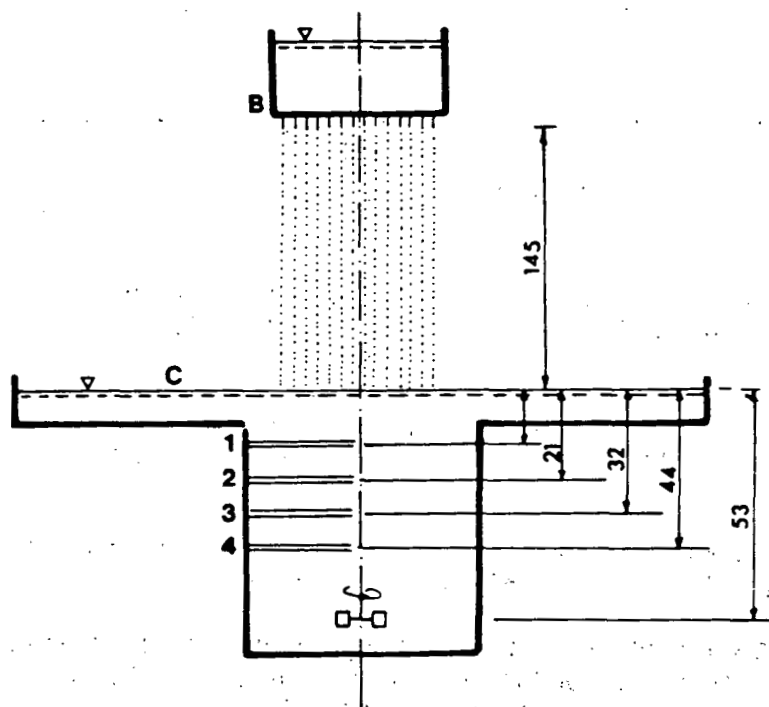


Fig. 4.23. The receiving tank in the rain drop experiment.

being collected through the taps 1 - 4 where glass tubes go almost to the center of the tank. Thus water samples are collected at different depths and ought to reflect a possible vertical gradient in the concentrations of oil in the samples. Such a gradient is indicated by the photo of the tank emptied after one normal experiment. (Fig. 4.24) The oil clinging to the outside of the glass tubes is dependent on the size and frequency of the droplets hitting the tubes. The photo shows that much more oil is collected by the upper tubes than by the lower ones. A corresponding gradient in the concentrations measured in the samples is not present because it is obscured by the large variations one may have due to occasional pick up of large oil droplets during sampling. This is, of

course, a source of inaccuracy in the experimentation which might have been avoided by increasing the physical size of the apparatus or by taking ensemble averages over a large number of identical runs. With these remarks in mind one may turn to Table 4.2 where a survey is given

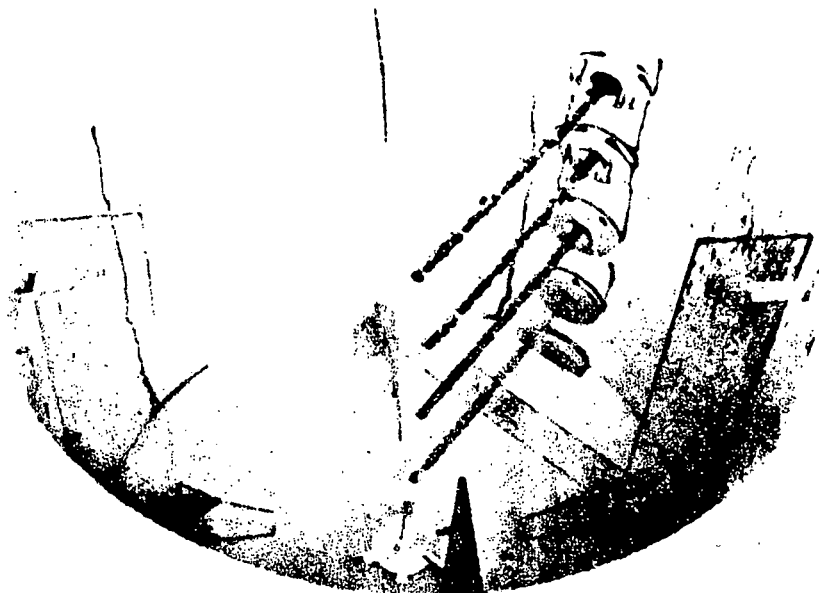


Fig. 4.24. Photo showing the gradient in the oil collected by the glass tubes.

over the variation of the parameters in the experiments. RD-7 through RD-18. In addition, the results of each experiment are shown in Figs. 4.25a-j as a record of the concentration of oil in the water column as a function of the time at which the samples were taken, the time $t = 0$ being the time at which the oil was applied to the surface. (A steady state of the rain as well as of the recirculating flow is assumed established beforehand). It should be noted that the size of the impeller as well as of the tank differ from those of the preceding section and no comparison can therefore be directly obtained between the two cases.

One may start the examination of the results by considering RD-11, RD-12, RD-14, RD-15, and RD-16 which all are cases where the rain has been stopped hours before the rotor was shut off. All of these show that regardless of the impeller speed (within the range of variation used) the concentration of oil entrained in the water column drops off dramatically as soon as the rain stops, i.e. as soon as the production of entrainable particles stops, even though the recirculating flow is maintained. Since the level of concentration reached after shutting off the rain is close to that after 24 hours one may conclude that in contrast to the drop size experiment the impeller speed is in this case kept so low that the recirculating flow does not contribute significantly to the production of entrainable particles. Its main effect is the transport of oil particles from the vicinity of the surface down into the water column. Apart from RD-14 this is a feature common to all experiments in this series, and it

Table 4.2 Experimental Parameters for Raindrop Experiments with Circulation.

No.	Amount of oil (ml)	Impeller Speed (rpm)	RAIN RATE (l/hr)		Rain rate (l/hr)	Temperature °C	Fall distance (cm)	Water	Surface tension	Drop Size (g)	Intentions	Remarks
			At beginning	At end								
RD-7	300	176.5 no further checks	-	-	-	-	148	Sea	-			
RD-8	300	178.8 no further checks	-	-	-	18° (room) 19° (water) at 0 hrs	148	Sea	-		Repeat of RD-7	cancelled
RD-8	300	169.1	3.48	-	3.32	3.87	18° at 0 hrs 20° at 8 hrs 22° at 24 hrs	Fresh	-	(.000011)		Drop size: .000011 g/drop (From RD-14)
RD-10	300	166.1 178 at break	3.57	3.80	-	-	27° at 0 hrs	Fresh	77.4 77.3 76.8	(.000011)	Sea water/Fresh water could not be distinguished based on surface tension	cancelled Drop size: .000011 g/drop (From RD-14)
RD-11	160	149.7 at 0 hrs. 171.8 at 8 hrs.	3.98	3.09	3.33	3.35	19° at 0 hrs 22° at 8 hrs	Fresh		.0000169		
RD-12	160	149.7 at 0 hrs. 159.3 at 8 hrs.	3.38	3.40	3.88	3.48 at 4.5 hrs. 4.33 at 8 hrs.	15.5° at 0 hrs (water)	Sea	76.0	.000017	Repeat of RD-11 (diff. water)	
RD-13	160	147.5 at 0 hrs. 164.7 at 8 hrs.	3.44	3.64	3.80	3.22 at 4.5 hrs. 3.69 at 8 hrs.	15° at 0 hrs 18° at 8 hrs 19.8° at 24 hrs	Sea	78.8 - 78.8	(.0000178)	Repeat of RD-12	Drop size from RD-14
RD-14	300	250.0 at 0 hrs. 259.7 at 8 hrs. 288.4 at 10 hrs.	1.92	3.13	-	3.88 at 24 hrs.	17° at 0 hrs 16° at 8 hrs 12° at 24 hrs	Sea	78	.0000118		
RD-15	160	158.1 at 0 hrs. 168.9 at 7 hrs.	3.10	3.02	3.04	3.33 at 2 hrs. 3.79 at 3 hrs. 3.03 at 4 hrs. 3.84 at 5 hrs.	8° at 0 hrs 10° at 8 hrs 10° at 24 hrs	Fresh	76	.0000178	Repeat of RD-11	
RD-16	300	169.0 at 0 hrs. 168.7 at 8 hrs. 166.7 at 8 hrs.	3.83	3.82	3.73	-	10.8° at 0 hrs 13° at 11 hrs 10° at 24 hrs	Fresh	74.5(?)	.0000167	Repeat of RD-8	
RD-17	160	155.8 at 0 hrs. 174.4 at 8 hrs. 172.0 at 24 hrs	3.71	3.66 3.69	3.78	3.80	13° at 7 hrs. 15° at 24 hrs.	Sea	68.3	.0000181	Repeat of RD-12 (modified)	
RD-18	300	151.8 at 0 hrs. 174.4 at 7 hrs.	3.82	3.57 2.50	3.77	3.94	24°	Sea	64.4 (28°C)	.0000173	Repeat of RD-7	

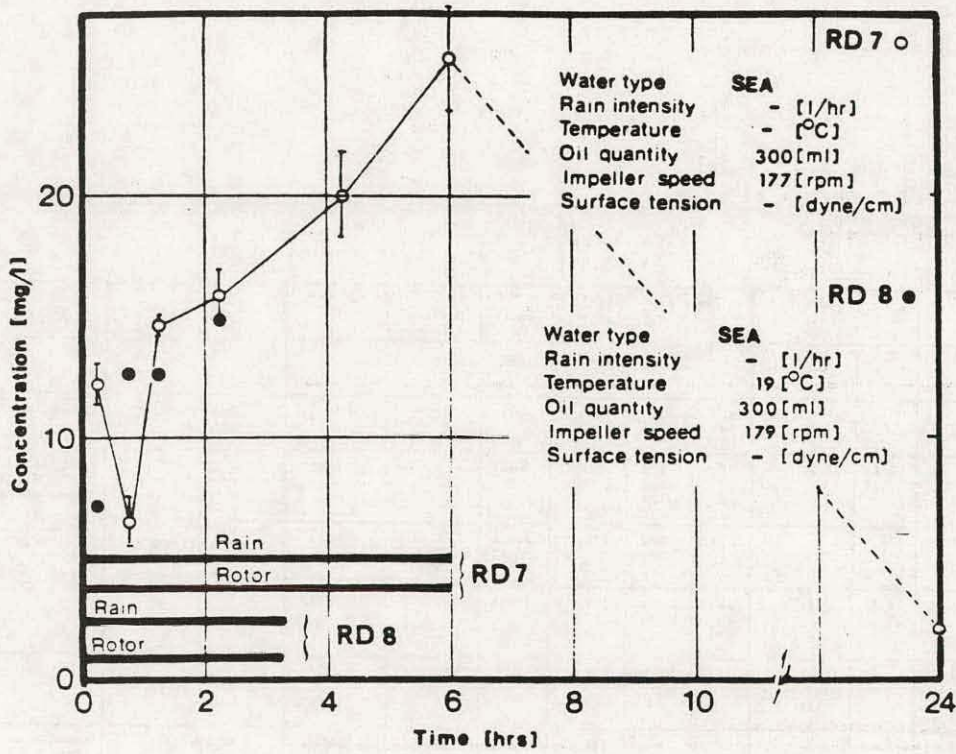


Fig. 4.25a

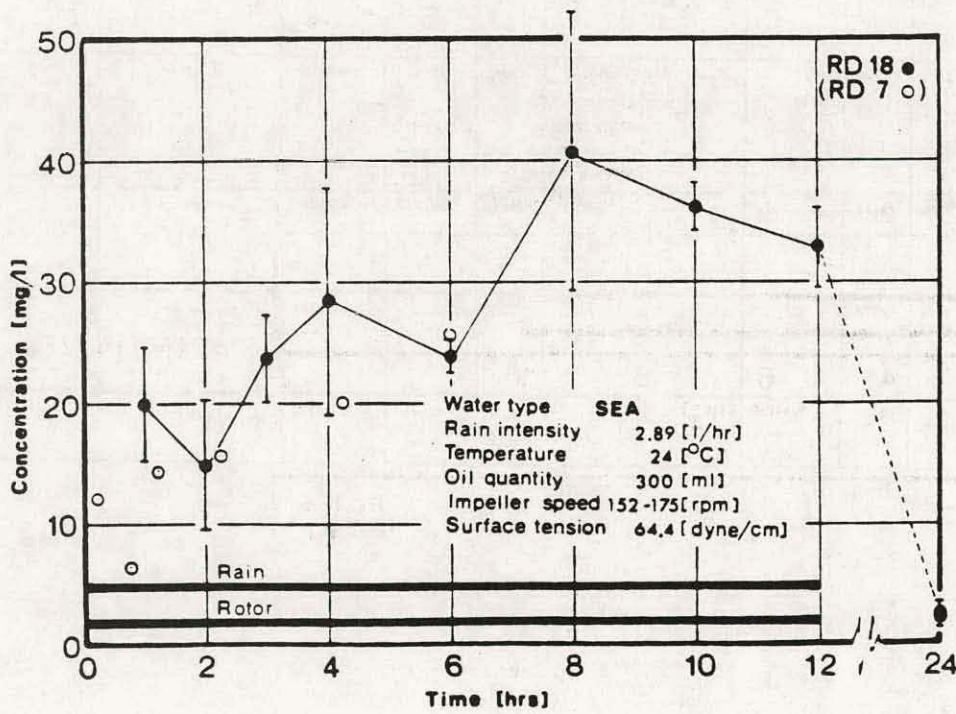


Fig. 4.25b

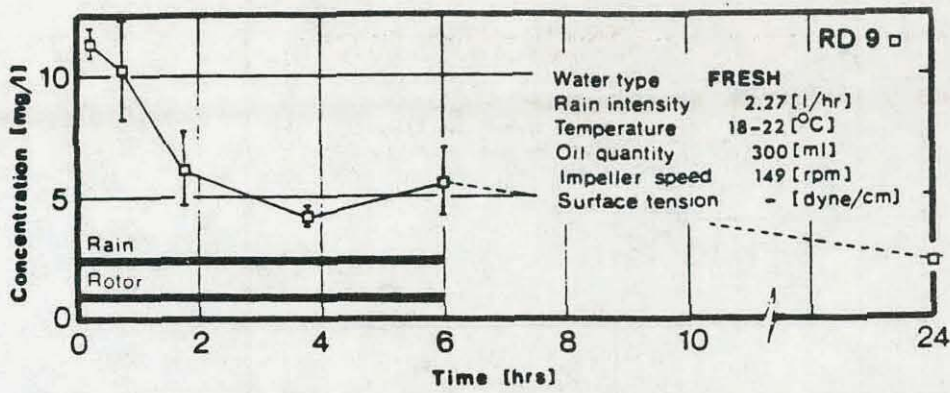


Fig. 4.25c

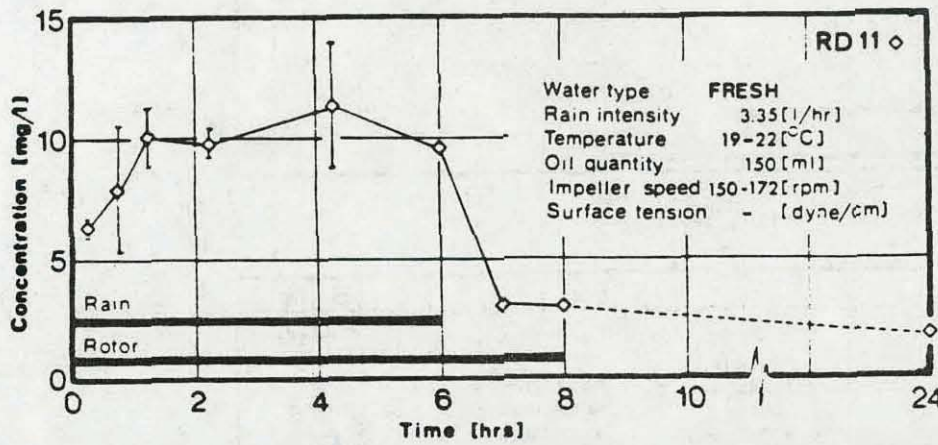


Fig. 4.25d

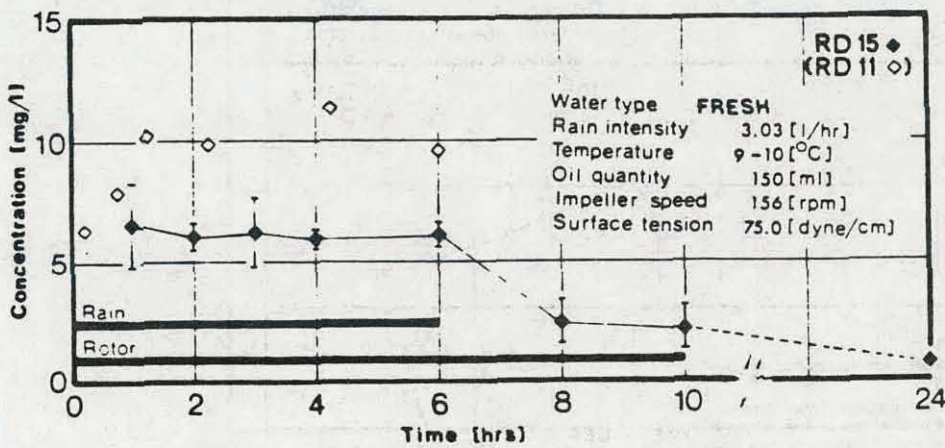


Fig. 4.25e

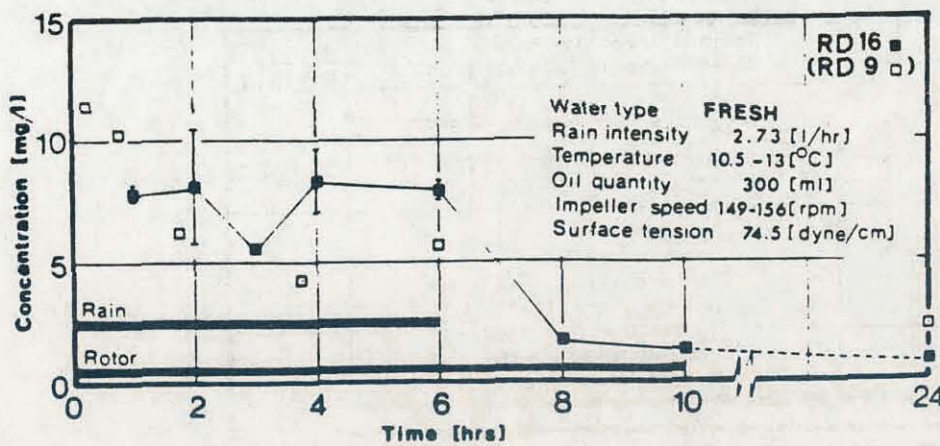


Fig. 4.25f

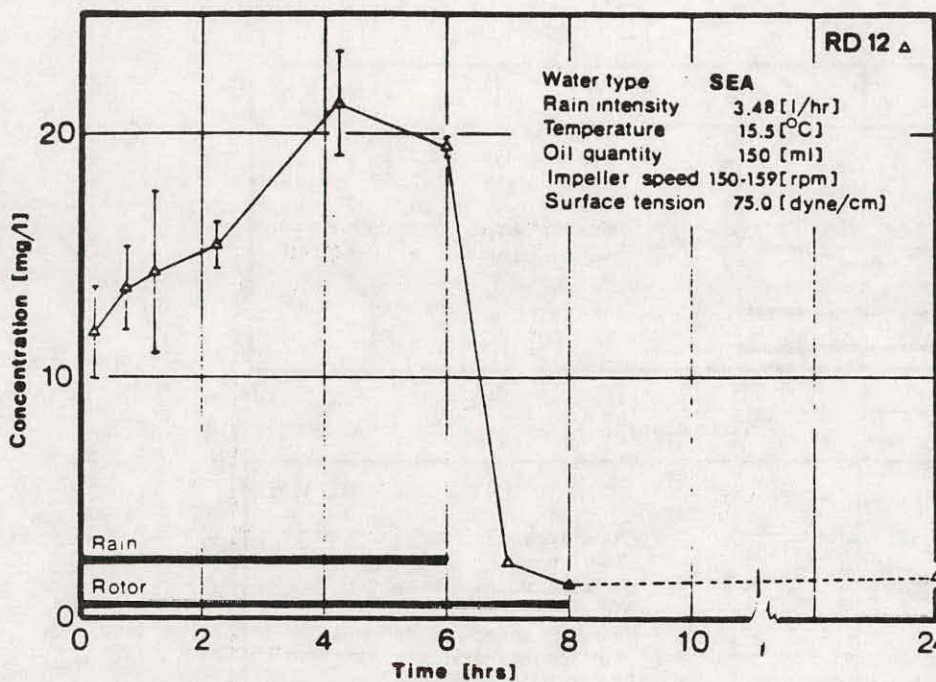


Fig. 4.25g

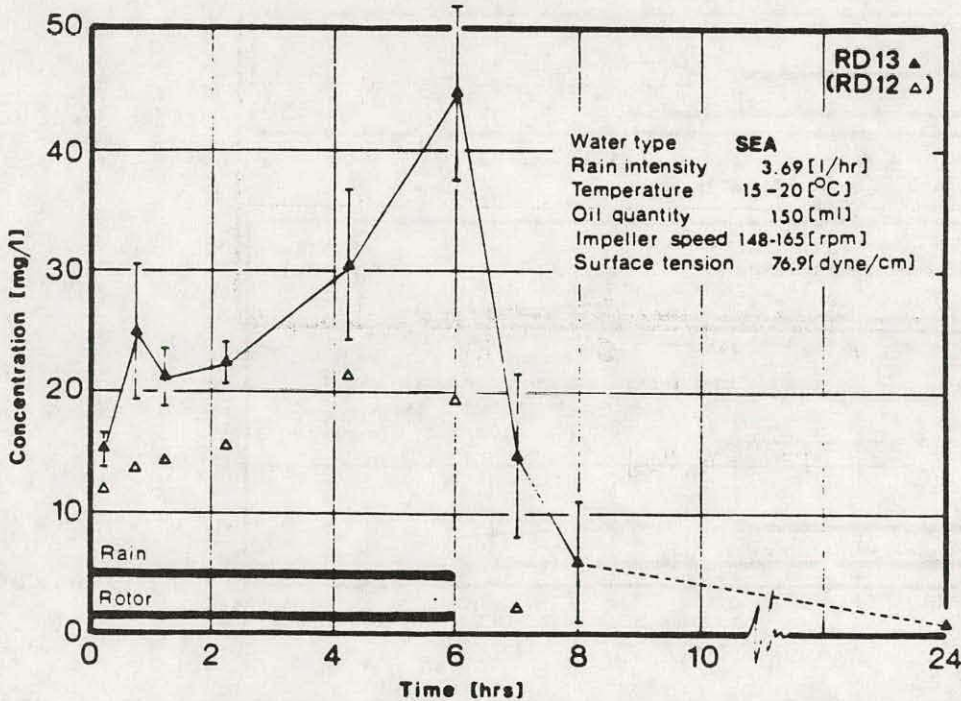


Fig. 4. 25h

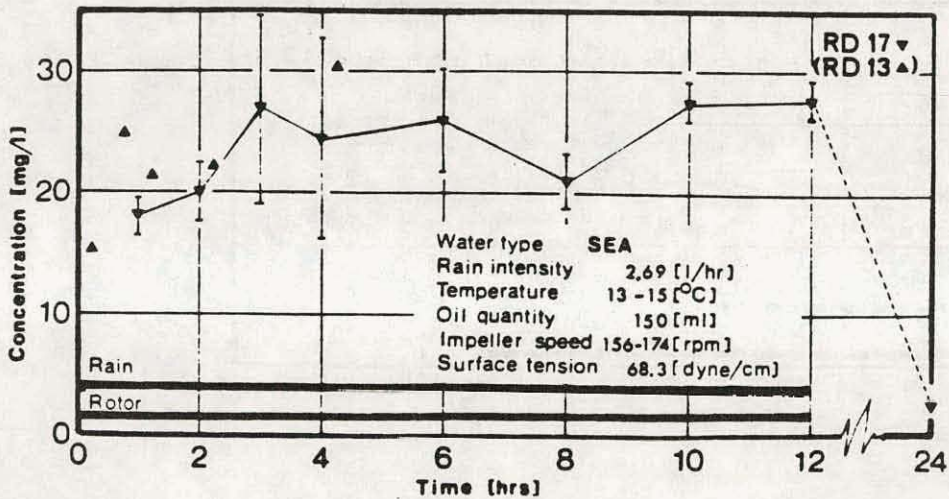


Fig. 4.25 i

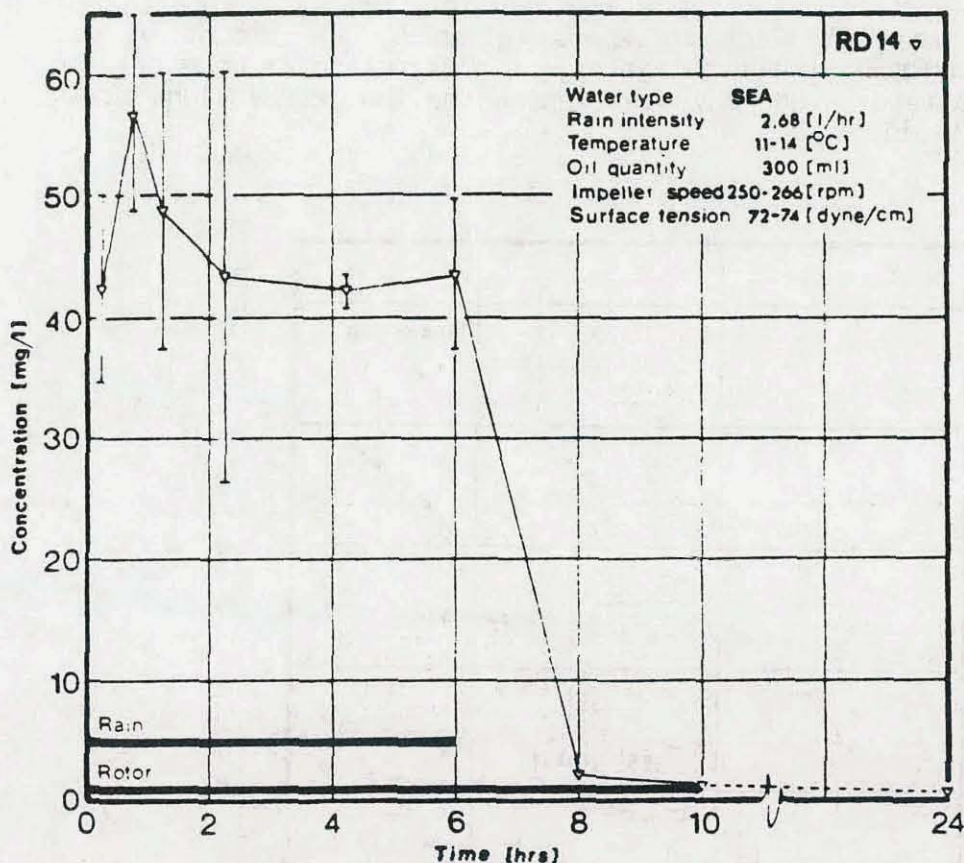


Fig. 4.25j

makes the impeller speed rather unsuited as a parameter. The results can then be used to explore the influence of other parameters such as temperature, slick thickness, etc.

One more comment ought to be given at this point. The entrainment is seen to drop off dramatically when the rain stops, but the same is observed when the rain continues and the impeller stops. This latter case is investigated by Dr. Cornillon and Ted Kawazoe and the result is given in a internal report by Ted Kawazoe.

Fig. 4.26 gives a survey of the results. The average concentration c of oil in the water column after 6 hours is plotted as a function of temperature with the oil slick thickness (given by the amount of oil applied to the surface) as the parameter. A distinction is made between tap water and sea water. One may now examine the four conclusions drawn in the preceding section.

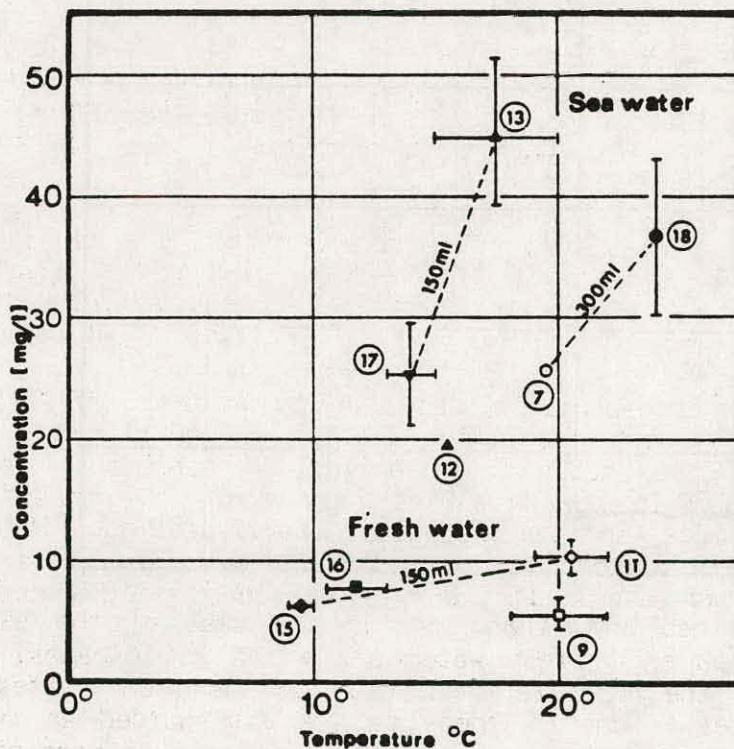


Fig. 4.26. Results of the rain drop experiment 6 hours average concentration plotted as function of temperature.

First, it is confirmed that irrespective of what type of water is used, the entrainment is higher for a thin slick than for a thick one. Conclusion 2 is thus supported.

Second, oil is seen to be much more easily entrained in salt water than in fresh water. This is in contrast to the result in the preceding section, Conclusion 3, and will be commented on in the next section, Final Remarks.

Third, Conclusion 4 of the preceding section cannot be reconsidered here because the influence of the recirculating flow on the production of entrainable particles is totally overshadowed by the action of the rain for the impeller speeds used.

Fourth, the influence of temperature, Conclusion 1 in the preceding section, is here exhibited in Fig. 4.26. It is seen that apparently a weak influence of temperature on entrainment is found in fresh water but an apparently very strong dependence is found in sea water. It is however felt that further experimentation would be needed to form a fixed opinion on this point.

4.4.5 Final Remarks

Summing up the results of these experiments one should not hide the scarcity of information they give and the corresponding uncertainty in the conclusions one may draw. However, some results seem to be fairly well established.

1. In all cases the original concept of entrainment being brought about by one action producing entrainable particles and another action (the recirculation flow) transporting the particles down into the water column has been supported. No evidence to the contrary could be detected.

2. The mechanism responsible for the production of entrainable particles in the rain drop experiment is the action produced by the impinging drops. This action is basically different from the corresponding mechanism in the drop-size tank where the production is caused by the vortices in the turbulent recirculating flow. This difference may be the reason for the apparent discrepancy as regards Conclusion 3 in the two cases. If the evidence for forming an opinion on Conclusion 3 is examined one finds that in the case of the drop size experiment it is based on 3 fresh water and 4 sea water cases. In the rain drop experiment the opposite conclusion is based on 4 fresh water and 4 sea water cases. None of these can be disregarded as "wrong." Thus it is possible that whether or not entrainment occurs more easily in fresh water than in sea water really depends on the mechanism whereby entrainable particles are being produced.

3. Conclusion 2 seems to be fairly well documented and corresponds also to the general picture.

4. The influence of temperature was never really systematically investigated and the last paragraph of the preceding section really expresses the situation fairly well.

4.5 EXPERIMENTS WITH APPLICATION OF THE DISPERSANT COREXIT 9527

4.5.1 Introduction

The influence of a dispersant on the entrainment process was intended

to be investigated through application of the chemical during a process which has been investigated previously without such application. It was decided to use only Corexit 9527 as a dispersant and to spray it on to the oil slick in a ratio Corexit/Oil = 1:20. This does however not mean that when hydrocarbons are recovered in the water column this ratio will persist between the part originating from the dispersant and the other part originating from the oil. One task will therefore be to establish a method which rather rapidly can determine this ratio, and this has been accomplished and is reported on elsewhere (see Section 12.2, Appendix B).

It is recalled that all cases reported on here (drop size experiment as well as rain drop experiments) have shown that when the recirculating flow is stopped, the amount of permanently entrained oil in the water column is negligible. A second task for this part of the investigation is to ascertain whether or not this feature, valid for oil only, is affected by the application of a dispersant.

A third important task is to investigate whether or not the application of a dispersant can enhance the entrainment of oil in the water column in the absence of a recirculating flow. One would then have a situation whereby the mechanism of entrainment from being caused by mechanical action is changed to being caused by what might be interpreted as molecular diffusion. The importance of one as compared with the other becomes an interesting question.

4.5.2 The Still Water Experiment

The last problem mentioned in the introduction was investigated in the still water experiment. The tank of the rain drop experiment was filled with sea water and left for 24 hours to let any motion in the water die out. An oil slick of known magnitude was then applied to the surface of the water in the tank. Great care was taken so as to avoid inducing any motion in the tank. After four hours samples were taken in the water column to see how oil alone might have diffused. Immediately afterwards the dispersant was sprayed on to the slick and samples from the water column were taken two hours and seven hours later. All samples were taken through the usual taps in the containers (Fig. 4.20) and they were taken so slowly that no appreciable velocity was induced in the water column. The following data give the details of the experiment:

Oil added: 62.68 [gr] to still Sea Water

Corexit - Sea Water mixture: 9.49 [gr] Corexit

95.28 [gr] Sea water

Of this mixture 29.69 [gr] was sprayed on the slick giving an applied amount of Corexit = 2.68 [gr]

Ratio Corexit/Oil = $r = 0.04280 = \underline{1:23.4}$

Temperature: 27° - 28°C

Since this case also serves as a test case for the determination of the

ratio $r = \text{Corexit/Oil recovered in the water column}$, the details of the evaluation is here shown in Tables 4.3 and 4.4. The samples taken are numbered, the time when they were taken is given, the taps from which they originate are indicated together with the legend used in Fig. 4.27 to display the results of each aliquot which also is numbered (i). The actual recovered amount of each aliquot is given as well as the transmittance z and the absorbance a obtained by scanning each aliquot at a wave number of 2930 $[\text{cm}^{-1}]$. Finally, the volume of each sample is given, and this concludes the data of the experiment. The values of z and a appearing in parenthesis are obtained in the region where the spectrophotometer is uncertain and are data which are not considered.

First, samples 1 and 2 contain only oil, no dispersant having been applied when they were taken. Thus, the ordinary calibration coefficient may be used and the concentration c_0 (shown in the column for $c_{C,i}$) is, at both tap 3 and 4, of negligible magnitude. Thus, even after four hours not very much oil has diffused into the water column. It is seen that only one aliquot was necessary to establish this result.

Table 4.3 SEA WATER

No	Time	Tap	Aliquot no. i	Recovered g	Transm. z	Absorb. a	Sample vol. ml	$c_{C,i}$ mg/l CCl ₄	$c_{C,i}$ mg/l H ₂ O	Computed	
										$c_{C,i}$ mg/l H ₂ O	$c_{C,tot}$
1	1:50 pm	3	1	46.74	89.5	.088	488	4.09	.24		
2		4	1	46.92	81.5	.089	482	7.64	.45		
3	4:15 pm	3	1	46.82	(18.0)	(.888)	475			4.81	
			2	47.40	28.0	.653		(43.13)	(6.88)	3.07	
			3	46.50	22.2	.206		31.01	1.92	1.96	
			4	47.40	75.5	.122		18.35	1.16	1.25	
			5	46.97	80.8	.093		18.92	.87	.79	
				253.86					11.87	18.18	
4		4	1	46.25	22.0	.658	502	(48.88)	(6.75)	2.82	
			2	46.66	36.7	.447		(47.27)	(3.94)	1.67	
			3	46.68	74.7	.127		19.05	1.12	1.06	
			4	47.34	84.0	.076		11.39	.68	.68	
			5	47.23	90.0	.046			.41	.43	
				253.96					6.46	9.85	
5	9:35 pm	3	1	46.16	(4.0)	(1.398)	479			3.06	
			2	46.80	(12.0)	(.921)				1.96	
			3	46.65	53.7	.270		(40.61)	(2.49)	1.25	
			4	47.06	81.5	.085		13.36	.83	.80	
			5	47.05	88.5	.053		7.98	.49	.51	
				253.72					7.61	11.65	
6		4	1	46.44	(3.0)	(1.523)	478	(46.32)		3.56	
			2	46.82	(10.0)	(1.000)				2.27	
			3	46.44	49.2	.308		(46.32)	(2.84)	1.45	
			4	46.80	78.7	.104		16.64	.97	.92	
			5	46.86	87.0	.060		9.09	.56	.59	
				252.16					8.79	13.46	
alt water			1	45.49			500				
			2	47.20							

Second, samples 3, 4, 5 and 6 contain oil and dispersant in a degree that could be detected with the naked eye. Five aliquots were applied successively and the result of scanning these is given. Now, if the assumption holds that the first 2-3 aliquots extracts the oil and only dispersant is present in the subsequent aliquots, then one may use the calibration curve for Corexit in these. This is shown in Table 4.3 and

displayed in Fig. 4.27, which show that indeed the latter aliquots gather around lines with a slope of -0.45 . These data are used to find the lines in Fig. 4.27 by linear regression.

Having these, not only the total concentration of Corexit ($c_{C,tot}$) in the sample can be computed but also the concentration $c_{C,i}$ of Corexit indicated by the i th aliquot. This is shown in Table 4.3 where also the sum giving $c_C^{(6)}$ is computed.

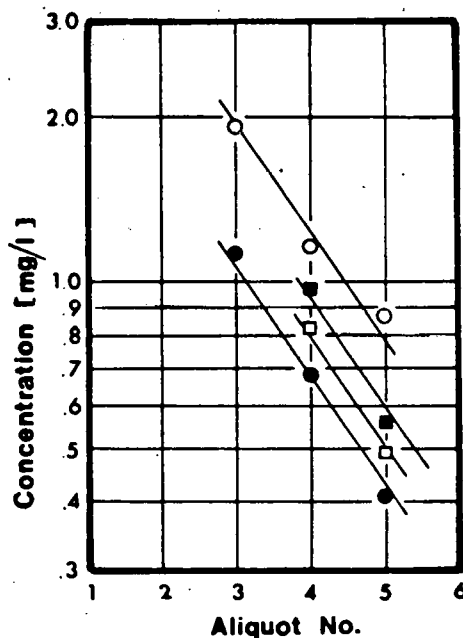


Fig. 4.27. Data shown to agree with the straight line behavior

In Table 4.4 one now proceeds to compute $c_C^{(6)}$ which is the concentration of corexit in the sum of all aliquots. When these are added and their sum is scanned at a wavelength of $2930 \text{ [cm}^{-1}\text{]}$ the absorbance a_m for the mixture is found. The iteration process previously described (see Section 12.2, Appendix B) will now render, and since the total concentration $c_{C,tot.}$ is known it is easy to compute $c_{o,tot.}$ as well as $c_{tot.}$ as shown in Table 4.4

Table 4.4 Extraction of Oil and Corexit from Sea Water

No	$c_C^{(6)}$ [mg/l H_2O]	Total aliq. [gr]	$c_C^{(6)}$ [mg/l CCl_4]	a_m	r	$c_{C,tot.}$ [mg/l H_2O]	$c_{o,tot.}$ [mg/l H_2O]	$c_{tot.}$ [mg/l H_2O]
3	11.87	233.9	38.05	.3660	3.73	18.18	4.87	23.05
4	6.46	234.0	21.97	.2636	2.03	9.89	4.87	14.76
5	7.61	233.7	24.72	.5323	.73	11.65	15.97	27.62
6	8.79	232.2	28.68	.5850	.79	13.46	17.07	30.53

A tremendous enhancement in molecular diffusion is caused by the application of Corexit. This is independent of whether or not mechanical agitation of some sort is present. It is seen that whereas little oil and much Corexit is found after two hours, the situation has changed after six hours when the content of oil and Corexit seems to be evenly distributed in a ratio close to 1. This result will now be reconsidered in light of similar experiments.

4.5.3 The Drop Size Experiment with Corexit 9527

As mentioned in the introductory remarks, the influence of Corexit on the entrainment should be investigated by applying the chemical to a similar experiment that did not use it. Thus the experiment in the 20 gallon tank was planned as follows:

1. The rotor speed was supposed to be kept so low as to achieve a situation in which very little oil would be entrained from the slick. This was the situation in E 10/17 (tap water) even at a rather high ambient temperature, and an impeller speed of about 65 rpm was decided upon.
2. It was intended to let the experiment run without application of Corexit for approximately 6 hrs. to ensure that a semi-steady state had been reached. Samples were to be taken from taps 2 and 3 at 4 hrs., 5 hrs. and 6 hrs. after applying the slick to the surface (time zero).
3. Corexit would then be applied to the slick in a ratio 1:20 (total amount of Corexit: total amount of oil in the slick). Samples would be taken at 10, 11 and 12 hrs (after time zero).
4. At this time the impeller speed is to be increased to the usual 150 rpm and new samples are to be taken at 24 and 25 hrs. (from time zero).
5. Then the impeller is shut off and final samples are taken at 48 hrs. (after time zero).

The data of the experiment can be summed up as follows:

Water: SEA WATER

Impeller Speed: 64.2 - 150 rpm.

Temperature: 24^o - 27^oC

Oil quantity: 51.56 gr

Corexit Quantity: 2.89 gr (Ratio: 1:17.8)

Surface Tension: 69.72 dynes/cm

Table 4.5 Experimental Results with Corexit 9527 and Circulation

No	Time Hrs.	Ratio Corexit/Oil	c_c [mg/l H_2O]	c_o [mg/l H_2O]	$c_{tot.}$ [mg/l H_2O]	Remarks
1	0	0	0	.92	.92	Control Rotor Speed 64.2
2	4	0	0	.23	.23	Oil added at 0 Hrs.
3				.34	.34	
4	5	0	0	.18	.18	
5				.42	.42	
6	6	0	0	.10	.10	
7				.14	.14	
8	10	1.061	250.1	235.7	485.8	Dispersant added at 6 Hrs.
9		1.055	252.9	239.8	492.7	
10	11	1.626	274.2	168.6	442.8	
11		1.209	223.3	184.7	408.0	
12	12	1.191	276.0	231.8	507.8	
13		2.043	302.3	148.0	450.3	
14	24	1.438	218.5	151.9	370.4	Rotor Speed increased to 150 rpm at 12 Hrs.
15		1.233	236.1	191.4	427.5	
16	25	1.312	218.6	166.6	385.2	Rotor stopped at 25 Hrs.
17		1.321	198.3	149.2	347.5	
18	48	2.167	271.5	271.5	396.8	
19		2.903	249.8	86.0	335.8	

The results of the experiment are shown in Table 4.5 and Fig. 4.28. In the latter the mean value of the concentrations at taps 2 and 3 is plotted against time. The results can be summed up as follows:

- The initial impeller speed is so low that very little oil is being entrained.
- The addition of Corexit causes a tremendous increase in entrainment.
- Changing the impeller speed has very little affect on the amount of entrained hydrocarbons.

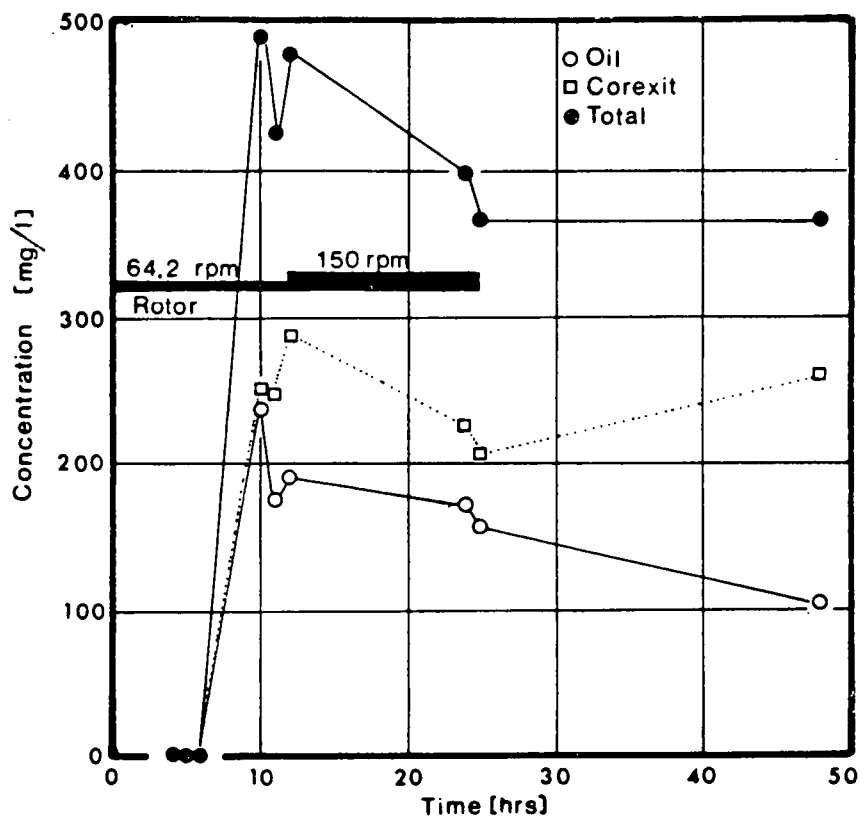


Fig. 4.28. Results of the drop size experiment with Corexit.

- d. The amount of hydrocarbons still being entrained 24 hrs. after shut-off of the impeller indicates a very high degree of permanently entrained particles in contrast to the cases with oil alone.
- e. The ratio Corexit/Oil in the samples is close to 1 but have a tendency to increase with time (after shut-off).

These results will be reconsidered in view of the results from the rain-drop experiment.

4.5.4 The Rain-Drop Experiment with Corexit

The basic philosophy behind this experiment is the same as explained in the previous case. The conduction of the experiment may be outlined as follows:

1. The apparatus is started up with the rainmaker as well as the rotor operating such that when the oil is applied to the surface, a semi-steady situation is present.
2. Oil is applied to the surface at time zero.
3. Samples are taken from taps 3 and 4 at 4, 5 and 6 hrs.

4. At 6 hrs. Corexit is applied to the slick in a ratio 1: 20 (i.e., mg Corexit: mg oil in the slick 1:20).
5. Samples are taken at 10, 11 and 12 hrs. from the same taps.
6. At 12 hrs. rotor and rain are shut off.
7. At 36 hrs. final samples are taken from the same taps.

The parameters of the experiment are:

Water type: SEA WATER

Rain Intensity: 2.74 l/hr.

Temperature: 26.5° - 29.8°C

Oil Quantity: 300 ml

Impeller Speed: 148.5 - 167.6 rpm.

Corexit Quantity: 12.5 gr (Corexit/Oil = 1:19.99)

The results of this experiment are found in Table 4.6 and displayed in Fig. 4.29. In the latter the mean value of the concentrations of

No	Time [Hrs.]	Ratio Corexit/Oil	c_c [mg/l H ₂ O]	c_o [mg/l H ₂ O]	$c_{tot.}$ [mg/l H ₂ O]	Remarks
1	4	0	0.0	39.1	39.1	
2			0.0	22.5	22.5	
3	5	0	0.0	18.7	18.7	
4			0.0	17.4	17.4	
5	6	0	0.0	14.8	14.8	Corexit added at at 6 hrs. after sampling
6			0.0	13.1	13.1	
7	10	.619	159.1	257.1	416.2	
8		1.036	162.1	156.5	318.6	
9	11	.781	153.0	195.8	348.8	
10		.793	138.2	174.1	312.3	
11	12	.890	135.6	152.3	287.9	Rain and rotor shut off at 12 hrs.
12		1.122	134.1	119.6	253.7	
13	36	2.289	135.6	59.3	194.9	
14		2.457	140.6	57.2	197.8	

Table 4.6 Results of Rain Drop Experiment with Corexit

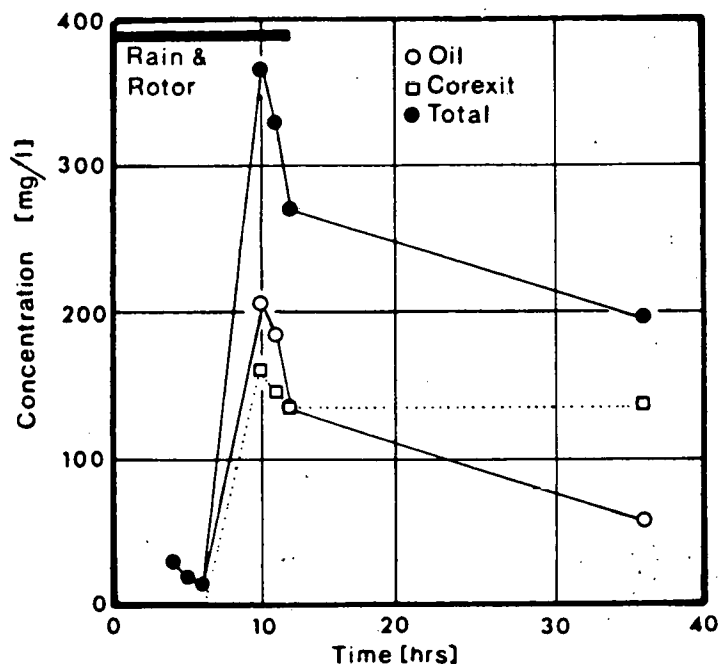


Fig. 4.29. The results of the rain drop experiment with Corexit 9527 applied.

the two taps is shown as a function of time. The results may be summed up as follows:

- A. The entrainment achieved by the rain and the recirculating flow within the first 6 hrs. is of the order of magnitude as in RD-18 and thus the previous results are confirmed (Fig. 4.25b).
- B. The entrainment obtained after application of Corexit is orders of magnitude larger than before.
- C. The ratio between Corexit and oil recovered in the samples is close to 1 but increases to about 2, 24 hrs. after shut off.
- D. The seemingly "permanently" entrained hydrocarbons (from oil and from Corexit) is almost independent of the physical situation under which the entrainment was achieved.

4.5.5 Final Remarks

The present experimental investigation has supported the ideas advanced originally by the author to explain the physics of the entrainment process. Thus the importance of the recirculating flow has been effectively demonstrated. Also the importance of the production of entrainable particles has been exhibited, but the influence of temperature is not satisfactorily explored. A difference in the way in which oil is being entrained in fresh water as compared with sea water has been demonstrated. However, the possibility exists that the way in which entrainable particles are being produced may influence the entrainment. Thus the apparent discrepancy between entrainment in the two cases (Figs. 4.22 and 4.26) may be explained. It is however stressed that further experimentation on this point is highly desirable. (See Final Remarks, Section 4.4)

The application of Corexit 9527 to the oil slick has a dramatic effect. Both from the drop-size and the rain-drop-experiments one may draw the conclusion that the effect of the mechanical situation (strength of recirculating flow, production of entrainable particles, etc.) is almost completely overshadowed by the effect of Corexit. This is brought out also by the fact that even in the still water case the entrainment is considerable. Attention in this connection is drawn to the fact that in Fig. 4.28 no apparent effect is found due to the change in the recirculating flow (impeller speed). One may draw the conclusion that the mechanism behind entrainment of oil into the water column is highly affected when Corexit is applied.

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5.0 Sample Application of the Oil Spill Model:
Georges Bank Oil Spill Simulations

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5.0 SAMPLE APPLICATION OF THE OIL SPILL MODEL: · GEORGES BANK OIL SPILL SIMULATIONS

5.1 Introduction

In this section, we describe the use of the oil spill fates model as a tool to analyze the effect of various treatment strategies on the fate of a simulated spill. The location of the spill was chosen at the center of the Cod spawning region on Georges Bank (Figure 5.1) and at a time, mid-winter, to affect a maximum impact on the Cod fishery. The output of the model resulting from these simulations was used as input to a fisheries model and is discussed in detail in Reed, Spaulding and Cornillon (1980) and Section 6 of this report. The discussion of these impacts will not be repeated here.

The size of the spill, 34,840 metric tons, as well as its duration, 39 hours, or spill rate, about 900 metric tons per hour (See Figure 5.2 for details of the spill characteristics) were chosen to correspond approximately to the Argo Merchant spill which occurred on Nantucket Shoals in December of 1977. The type of oil selected was a No. 2 like fuel oil also characterized in Figure 5.2.

Five different treatment scenarios were analyzed. By "treatment" we refer to application to the spill of chemical dispersants used to drive the oil on the surface into the water column. Although reducing the surface expression of the spill, such treatment will of course increase the concentration of hydrocarbons in the water column. The oil model has therefore been designed to follow the dispersed oil, and the surface slicks as well as to present the output in a convenient easy to understand graphical format. The five treatment scenarios examined in this section consist of one case in which no treatment was performed and four cases in which various fractions of the oil remaining on the surface were assumed to be driven into the water column, specifically, 25%, 50%, 75% and 100%. All treatment was assumed to take place 48 hours after the spill began, or approximately 9 hours after the last oil had leaked from the source. The various spill scenarios are outlined in Figure 5.3.

5.2 Environmental Variables

Environmental variables input to the model consisted of wind, water temperature and currents. The water temperature was assumed to be constant over the entire study area. The wind data were obtained from the Nantucket Airport Weather Bureau Station at three hour intervals. Missing wind data were obtained by linear interpolation between existing data points.

The current data were constructed from two sources. One source was the seasonal mean data of Bumpus (1973) (Figure 5.4). The data for a given season were assumed to apply only to the first day of that season. All other values were linearly interpolated between the two appropriate seasons. Bumpus' results were obtained from a long term surface drifter study, hence do not in general include short-lived wind induced currents (several days). These events were simulated by a two dimensional vertically averaged wind-current model using the Nantucket wind data as input. The wind induced currents were assumed to apply only to the

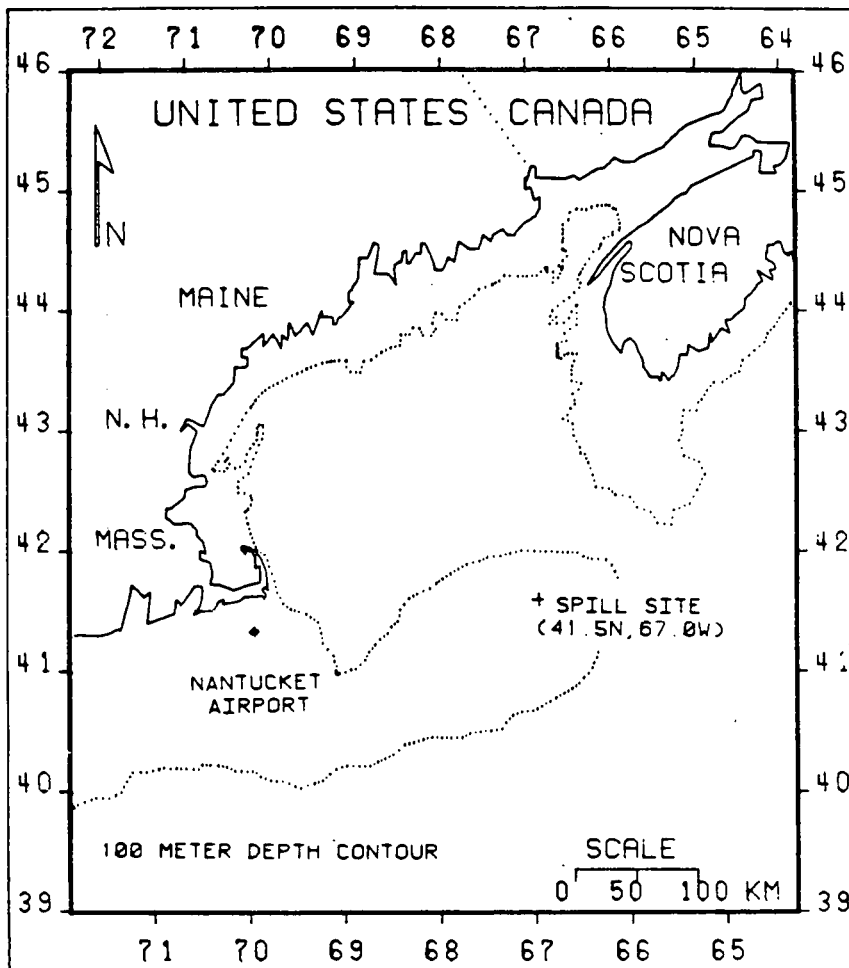


Figure 5.1 Location of Spill

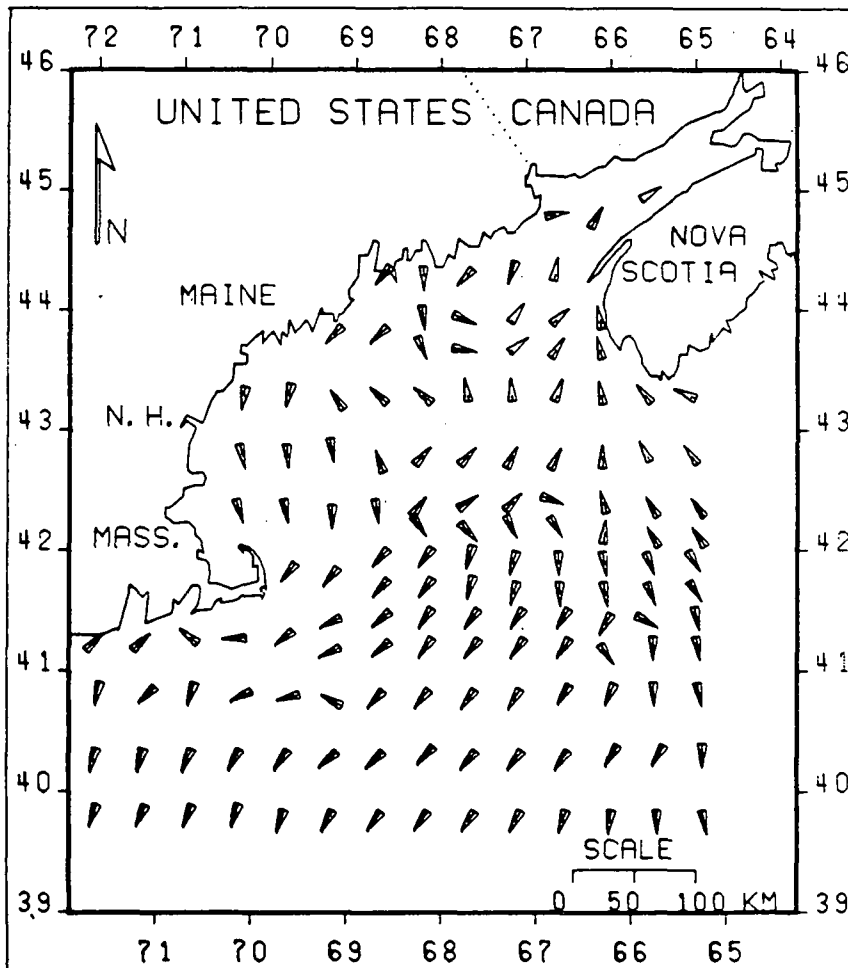
Figure 5.2: Model Input Parameters

Spill location	67°W longitude 41.5°N latitude
Thermocline depth	10 meters
Wind	December 1972
Temperature	December 9°C
Currents	Winter 1972
Oil	
Density	0.847 gm/cm ³
Interfacial tension	30 dynes/cm
Kinematic viscosity	1 centistoke
Oil fractions (by weight)	
Paraffin, C ₆ -C ₁₂	0.1
Paraffin, C ₁₃ -C ₂₂	0.25
Cycloparaffin, C ₆ -C ₁₂	0.15
Cycloparaffin, C ₁₃ -C ₂₂	0.15
Aromatic, C ₆ -C ₁₁	0.15
Aromatic, C ₁₂ -C ₁₈	0.05
Naphtheno-Aromatic, C ₉ -C ₂₅	0.15
Residual	0.0
Total	34,840 metric tons
Total number of spilletts	13
Oil spill rate	893.33 metric tons/hr
Total spill simulation time	30 days
Time step	3 hours
Horizontal dispersion coefficients	10m ² /sec

Figure 5.3 Cases Run

Case	Site	Wind Temp.	Current	Chemical Disp. After 48 Hours	Diffusion	Entrain	Length
1	Georges Bank	December	Bumpus plus wind induced	0 %	10 m ² /sec	Natural Advection plus Exponent. Decay	30 Days
2	same	same	same	25 %	same	same	same
3	same	same	same	50 %	same	same	same
4	same	same	same	75 %	same	same	same
5	same	same	same	100 %	same	same	same

Figure 5.4 Winter Currents



upper few meters (down to the thermocline in this case) of the water column. Details of the model are given in Reed and Spaulding (1979), and Section 6 and 12.5 of this report.

5.3 Natural Entrainment of the Spilled Oil

The process of primary interest in the impact analysis discussed herein is dispersion - both natural and chemical. For natural dispersion, which proved to be of significance in the case studied, the entrainment rate obtained by Audunson (1977) in the Bravo Blowout Study is used. Audunson's expression is:

$$\text{Fraction} = 0.1 \frac{(u^2)}{(w_0^2)}$$

where:

Fraction is the fraction by weight of the oil remaining on the surface to be entrained;

w_0 is a wind speed constant equal to 8.5 m/s

and

u is the measured wind speed at 10 m in units of m/sec.

For this model, Audunson's expression was modified by a factor decaying exponentially with time. The time constant used was two days. The intent of this term, selected in an ad-hoc fashion, is to incorporate weathering of the surface slick into the entrainment process. Often as the surface slick ages it becomes emulsified (water-in-oil) and is not as easily entrained as in the early stages. These effects may well have been masked in the derivation of the original equation for two reasons. First, the Bravo spill occurred over a fairly long period (weeks) so there was almost always fresh oil coming to the surface. Second, the crude oil involved in the Bravo spill did not appear to emulsify as readily as other oils.

In the case of chemical dispersion, a delay of 48 hours was implemented in the model before dispersants were applied. This delay was intended to simulate the time necessary to organize a treatment effort, and is, of course, a parameter that could be experimented with in future applications of the model.

The oil entrained is represented by marker droplets or particles. For each of the simulations discussed here, about 1900 droplets were used. Because the mass of oil in the water column varies from one scenario to the next and the number of droplets was fixed, the mass of oil represented by a marker droplet also varied from one scenario to the next. The particles were distributed randomly under the spill in the horizontal. In the vertical, they were assumed only to occupy the water column above the thermocline, 10 meters in this case. The particles were distributed randomly in these 10 meters.

5.4 Results

5.4.1 Mass Balance

The values of a number of variables of interest in assessing the various strategies are summarized in Table 5.1 for the last day of the simulation. Figures 5.5-9 show the mass balance as a function of time. The oil is very light so that about 40 percent evaporates within several hours of its release. The value is always within two percent of this even when all the oil is dispersed, case 5. Treatment earlier in time would of course decrease the mass to evaporate.

In case 1, no chemical dispersion, 8.6 percent of the original mass is entrained and the remaining 51 percent remains on the surface. These two values of entrained and surface mass increase and decrease, respectively, until, for the 100 percent dispersed case, 60 percent of the mass enters the water column, with none remaining on the surface. There is seven times as much oil in the water column for the totally dispersed case (case 5) as in the non-dispersed case (case 1). The mass distribution for all cases is identical for the period before any treatment.

5.4.2 Horizontal Area Over Which the Concentration exceeds the 50, 100 and 1000 ppb Predefined Values

Figures 5.10-13 are graphs of the horizontal area for which the oil concentration exceeds 50, 100 and 1000 ppb, respectively versus time. For the 50 ppb contours, the final area varies by 60 percent between the first three cases, but the last three high dispersed cases differ by only about 5 percent. For the 100 ppb and the 1000 ppb contours, only the last two dispersed cases are within 5 percent of each other. There is about a 10 to 20 percent reduction in the area covered when going from the 50 ppb contour to the 100 ppb contours. The area covered by the 1000 ppb contour is smaller in all cases. In the non-dispersed case, the final area for the 1000 ppb contours occurs at day 15 and the maximum concentration at day 30 is 476 ppb. The maximum concentration at day 30 for the dispersed cases exceeds 1650 ppb.

There are a couple of interesting points concerning these curves. First, for cases 2 to 4, the area which the 50 ppb contour covers is larger than the 100 percent dispersed case for the first 15 days. The areal extent for the 100 percent dispersed case does not exceed the others until between days 15 through 20. This is due to the natural dispersion which continues after treatment. The surface spilletts movement causes the naturally treated mass to be entrained further to the east than the treated mass and thus increases the area covered. The amount of mass entrained after treatment decreases with an increase in percent dispersed as a result of lesser amounts of oil on the surface. The maximum difference between areas due to this increase in area is 25 percent and occurs at day 5 between the 25 percent and 100 percent cases. The difference in areal coverage between these two cases decreases to 20 percent for the 100 ppb contour and is less than 3 percent for the 1000 ppb contours. The areal extent during this same period for the 100 percent dispersed case (50 ppb) is less than the 50 percent and 75 percent dispersed cases by 20 percent and 5 percent respectively. For the 100 ppb contour, the 50 percent and 75 percent dispersed cases at day 5 are within nine

Table 5.1 Data for Cases Run

% Disp.	% in Atmosphere	% on Surface	% in Water Column	Final Area (km ²) of Subsurface			ppb Highest Conc. at day 30
				50 ppb	100 ppb	1000 ppb	
0	40.2	51.2	8.6	1138	808	27 ¹	476
25	39.9	38.5	21.6	1505	1239	206 ²	1651
50	39.9	25.6	34.5	1701	1384	374	2774
75	40.7	12.8	47.5	1763	1491	577	4413
100	39.6	0	60.4	1792	1524	583	6257

MASS DISTRIBUTION

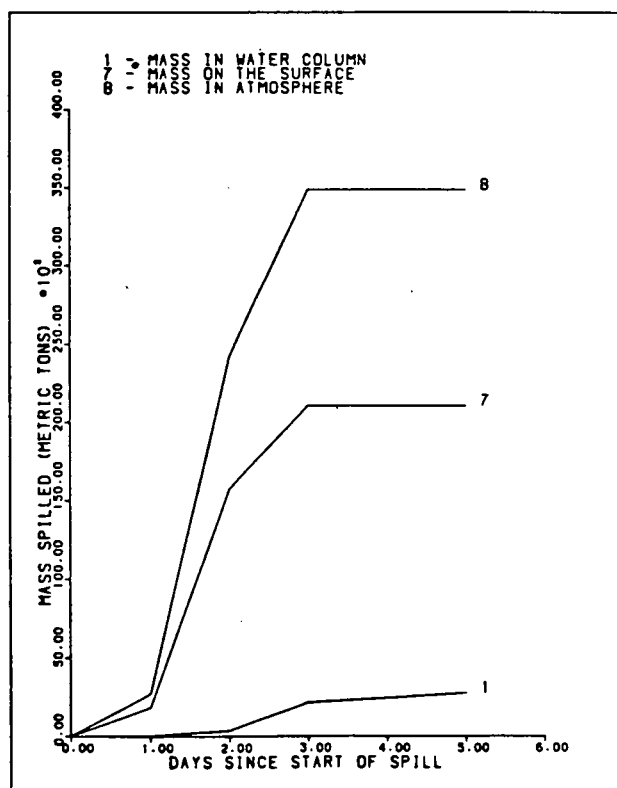


Figure 5.5 Mass Balance 0% Dispersed

MASS DISTRIBUTION

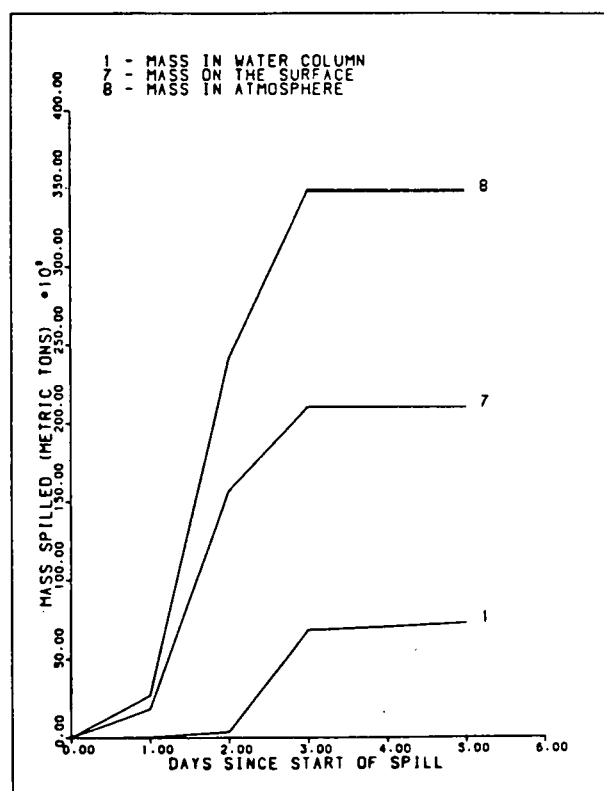


Figure 5.6 Mass Balance 25% Dispersed

MASS DISTRIBUTION

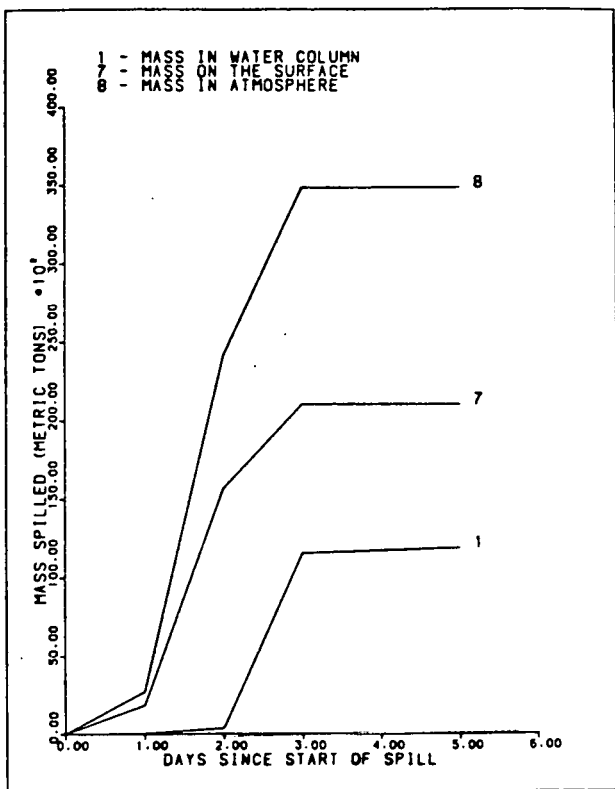


Figure 5.7 Mass Balance 50% Dispersed

MASS DISTRIBUTION

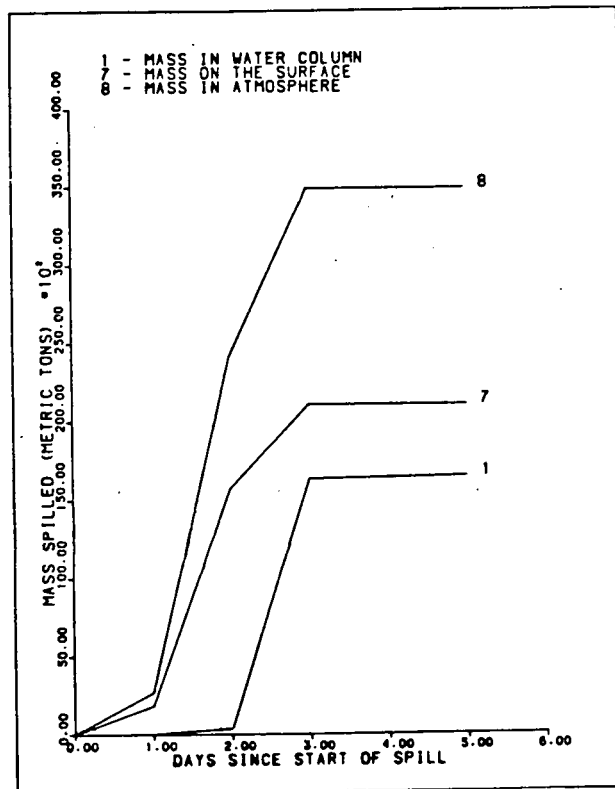


Figure 5.8 Mass Balance 75% Dispersed

MASS DISTRIBUTION

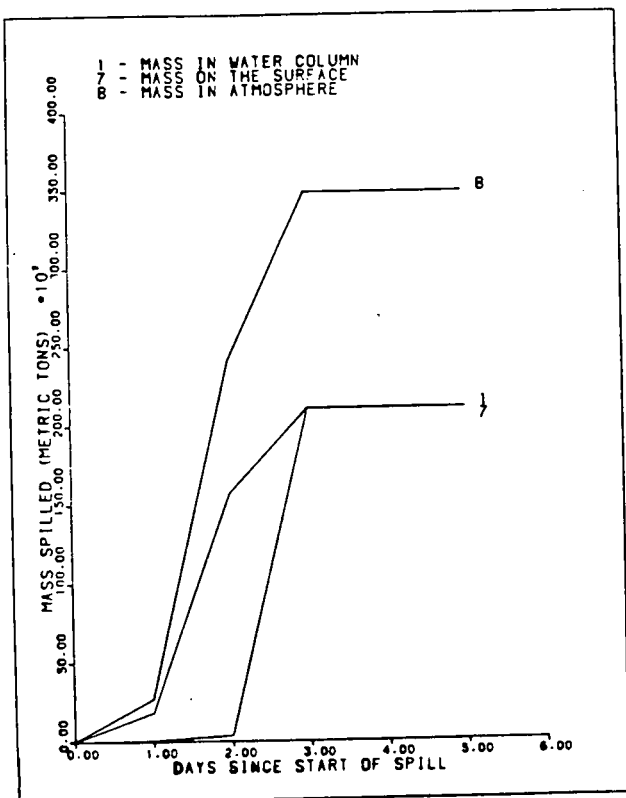


Figure 5.9 Mass Balance 100% Dispersed

AREA COVERED BY SPILL

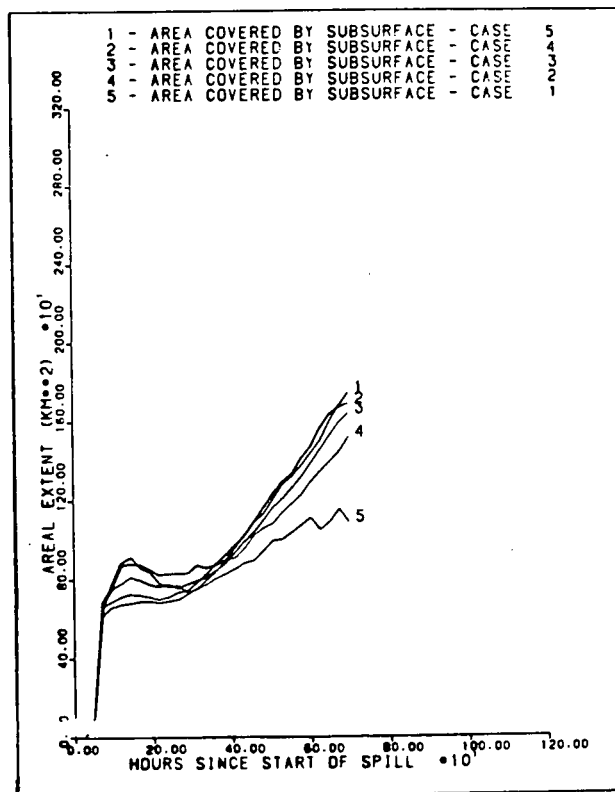


Figure 5.10 Areal Extent 50 ppb.

AREA COVERED BY SPILL

AREA COVERED BY SPILL

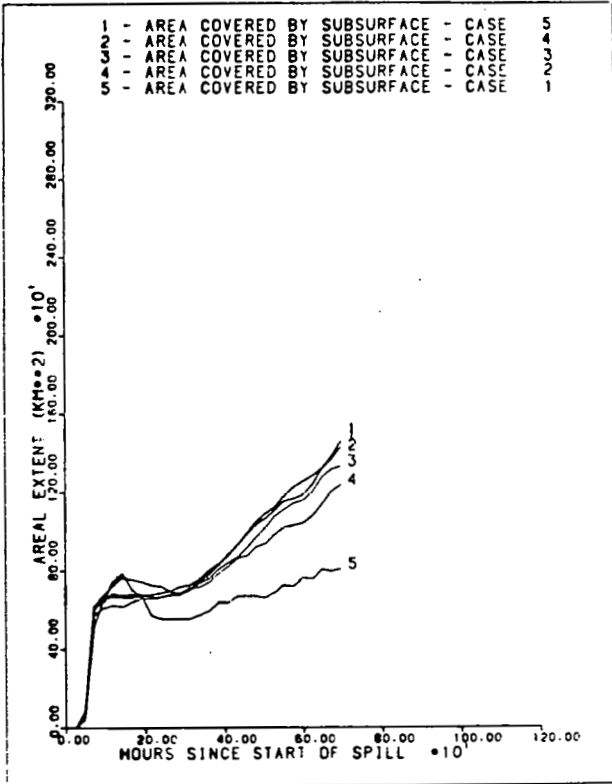


Figure 5.11 Areal Extent 100 ppb.

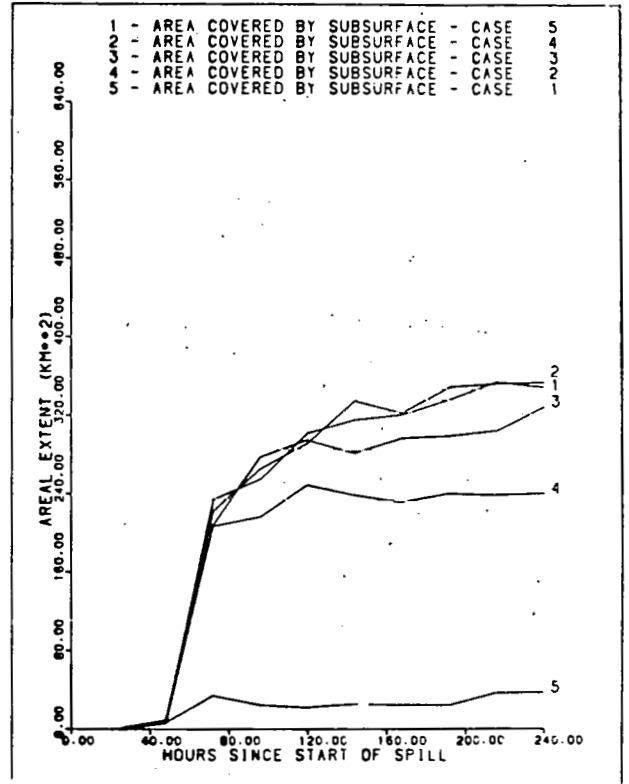


Figure 5.12 Areal Extent 1000 ppb. (10 days)

AREA COVERED BY SPILL

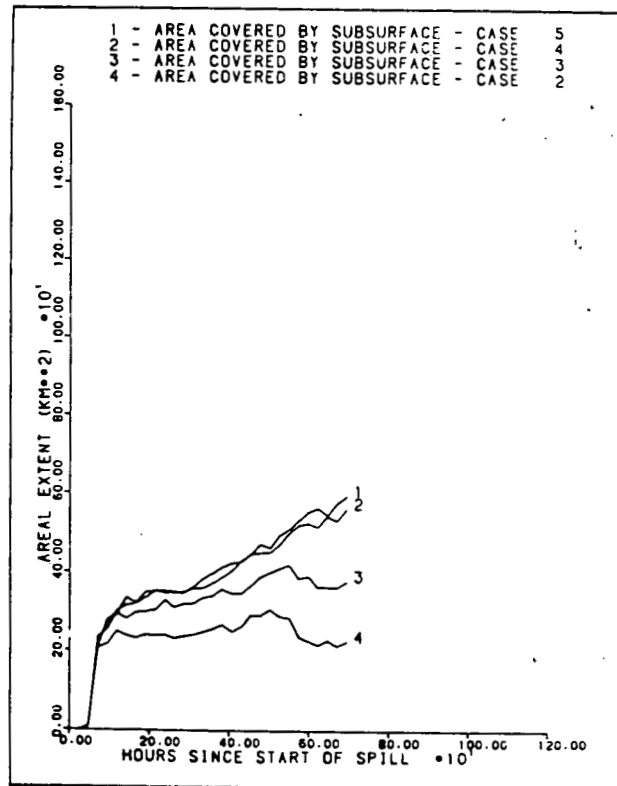


Figure 5.13 Areal Extent 1000 ppb. (31 days)

percent of the 100 percent dispersed case. As in the 50 ppb contour, the area of the 100 percent case is comparable to the other dispersed cases between 15 and 20 days after the spill for the 100 ppb contour. The 1000 ppb contours for all of the dispersed cases are very similar.

The other interesting feature of the areal extent curves is the decrease or leveling off of the area at approximately day 10 in most of the cases. This is due to the currents compressing the droplet cloud in the North-South direction. This is more noticeable in the 50 ppb contours and in the lower dispersed cases than in the higher contours and in the higher percent dispersed cases.

Charts including the contour lines and surface spills are included in Figures 5.14 through 5.24 for the 50 ppb, 100 ppb and the 1000 ppb lines. The non-dispersed case (case 1) is compared to cases 2 to 5 for the first two contours (Figures 5.14 to 5.17 for the 50 ppb contour and 5.18 to 5.21 for the 100 ppb contour) and the 25 percent dispersed case is compared to cases 3 to 5 in the 1000 ppb plots (Figures 5.22 to 5.24). In all of the views, the surface spillets have identical movements due to identical currents and winds for all of the scenarios. The wind blows from the west and shift to the north during the first five days resulting in the L-shaped pattern of the spillets. This causes the first spillet to move furthest to the east and the last spillet released to be to the south. The spillets move together to the southeast during the remaining time that the oil is tracked.

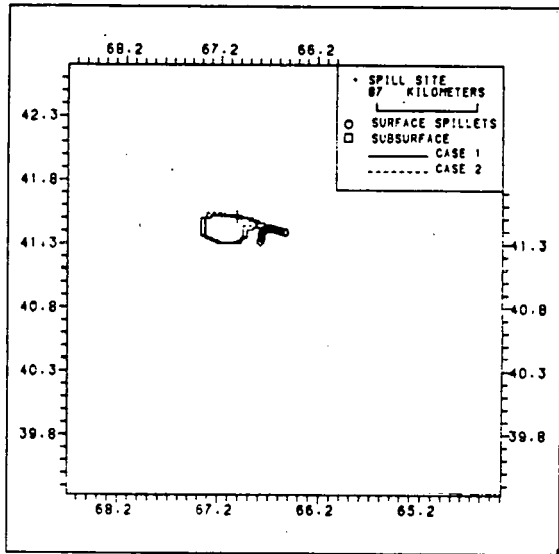
The movement and shape of the subsurface contours show some similar characteristics. The area covered by the non-dispersed case is larger than the other cases 5 days into the spill as was cited before. The compressive effect of the currents is shown clearly at day 10 for the 50 ppb outlines. The subsurface currents are generally southerly but the magnitude of the currents on the northern edge of the cloud are greater than those at the southern edge. This results in a collapse of the North-South dimension of the cloud as well as decreasing the areal coverage. As the cloud moves further south, the difference in currents is not as great and with the help of diffusion, the contour assumes a square shape at approximately day 15.

The plots for the 100 ppb contours show the same general behavior with the exception that the contours assume a more regular shape by day 10. The 1000 ppb contours are very similar as was the areal coverage.

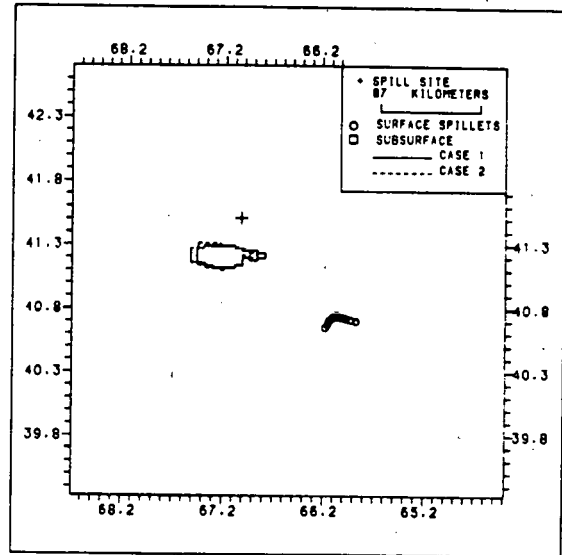
5.5 Conclusions

An open ocean oil spill can be simulated using the model developed and different response strategies can be investigated. The movement of the spilled oil dependent on environmental variables is of importance at the beginning of the spill for cleanup or treatment. The efforts must begin before the oil weathers or spreads, both of which would reduce the efficiency of any efforts. The spillets in these runs are spread out over an area greater or equal to four kilometers after 3 days, thus making any treatment or cleanup attempt difficult. The surface area covered is approximately 10-20 percent of the area covered by the subsurface 50 ppb contour. The surface area overlaid by the higher dispersed cases is greatly reduced by as much as a factor of 10 due to entrained mass.

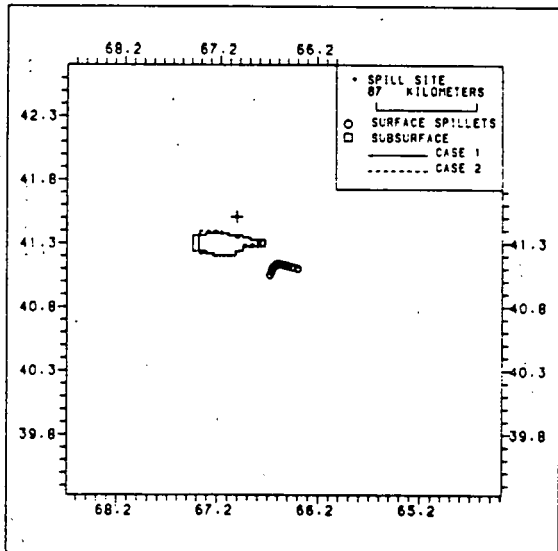
120.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE



360.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE



240.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE



720.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE

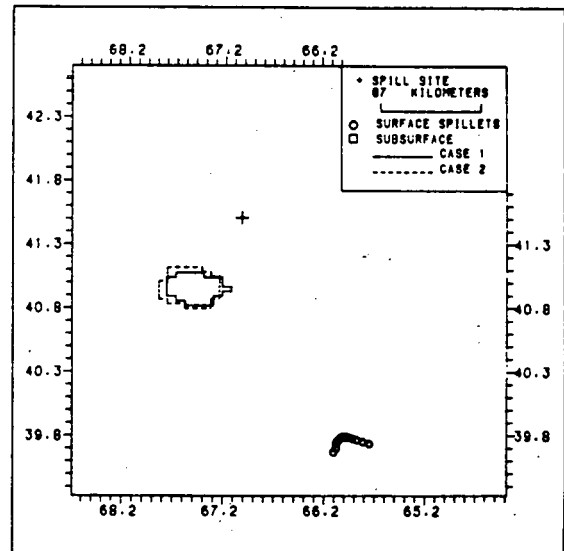
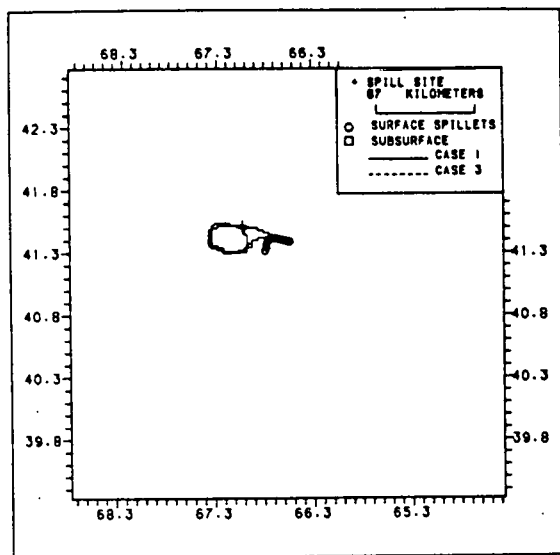
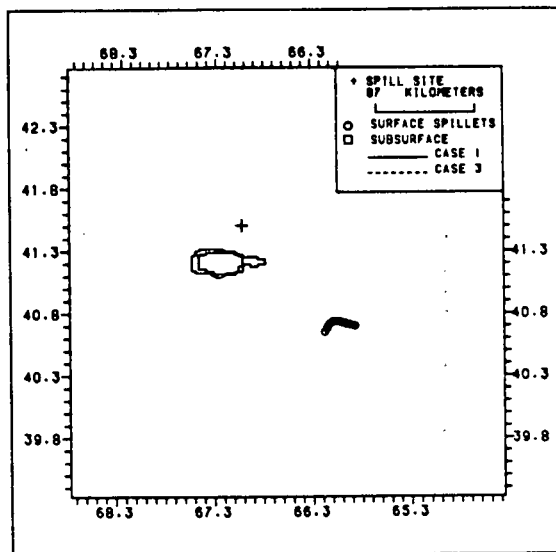


Figure 5.14 Overhead Views 50 ppb. Case 1 vs. Case 2

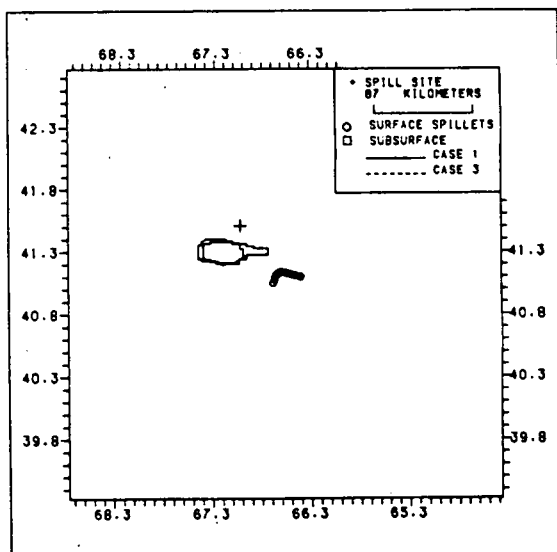
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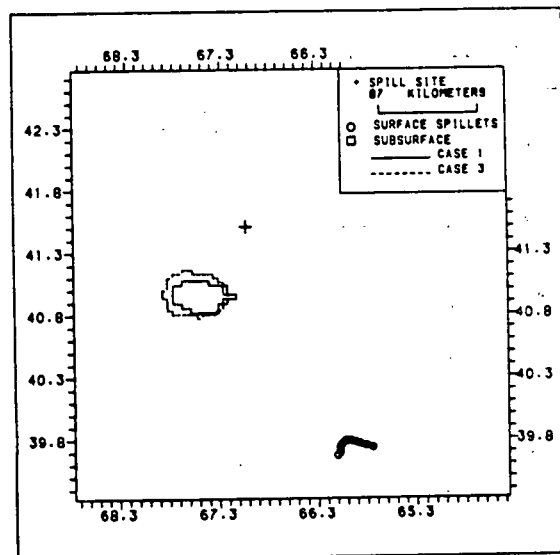
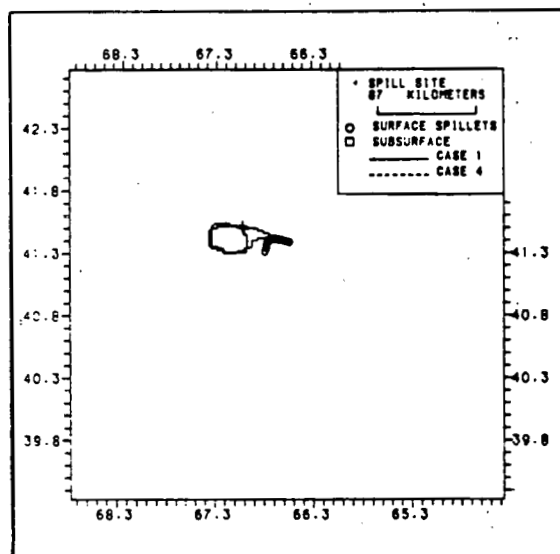
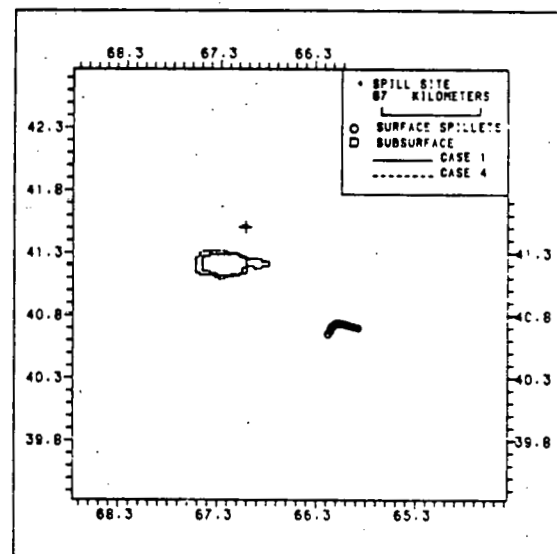


Figure 5.15 Overhead Views 50 ppb. Case 1 vs. Case 3

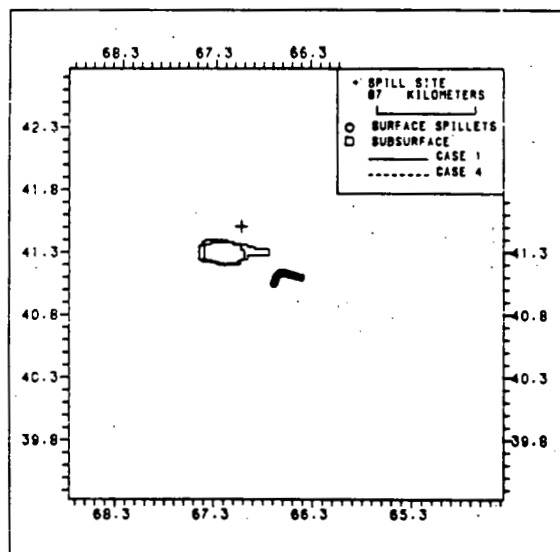
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720.0 HOURS AFTER START OF THE SPILL
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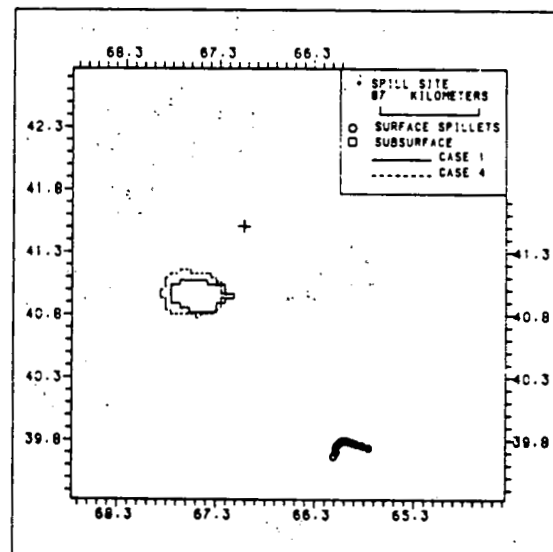
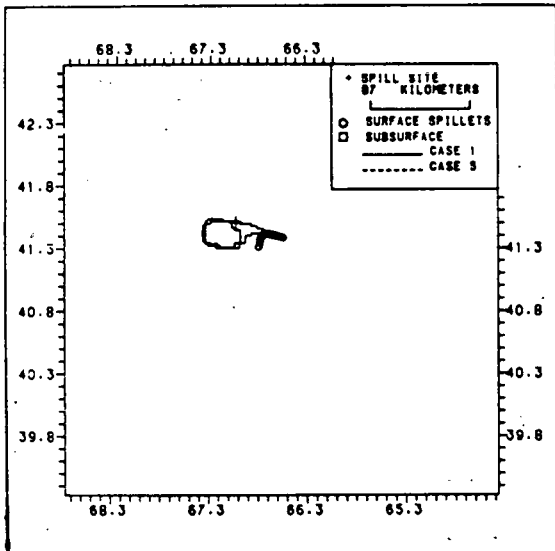
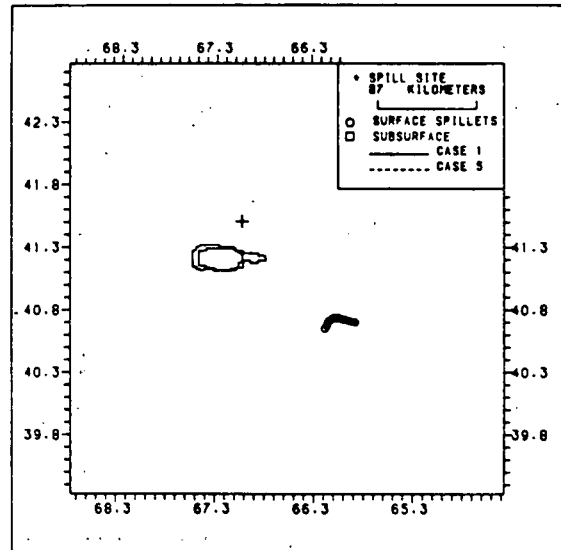


Figure 5.16 Overhead Views 50 ppb. Case 1 vs. Case 4

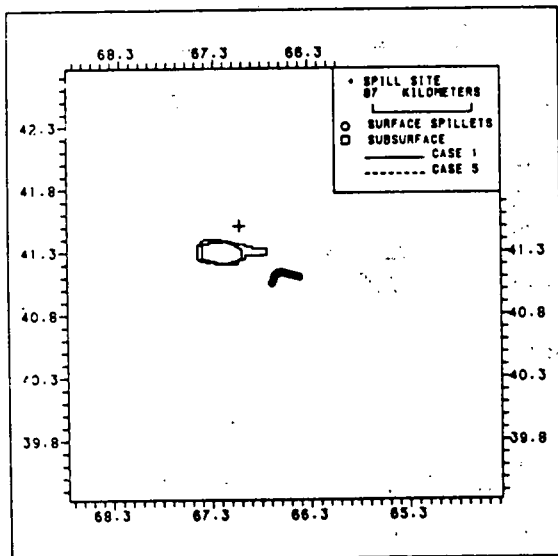
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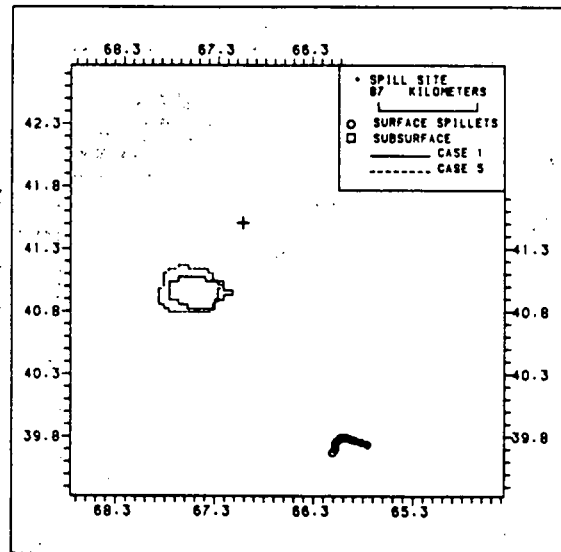
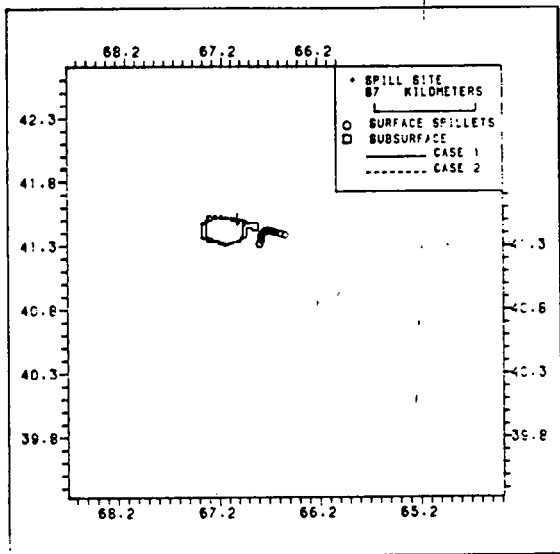
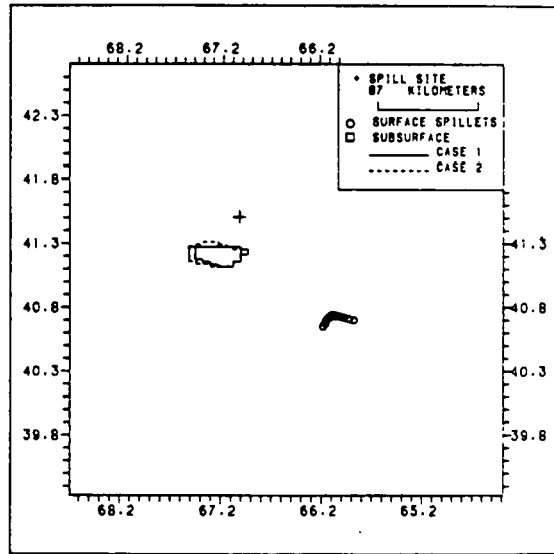


Figure 5.17 Overhead Views 50 ppb. Case 1 vs. Case 5

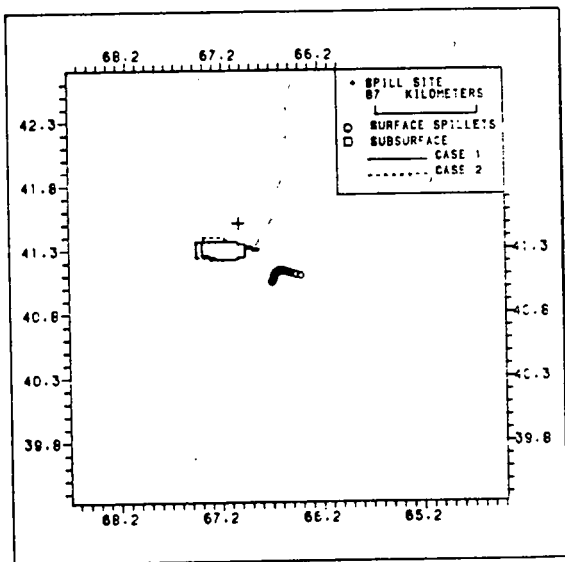
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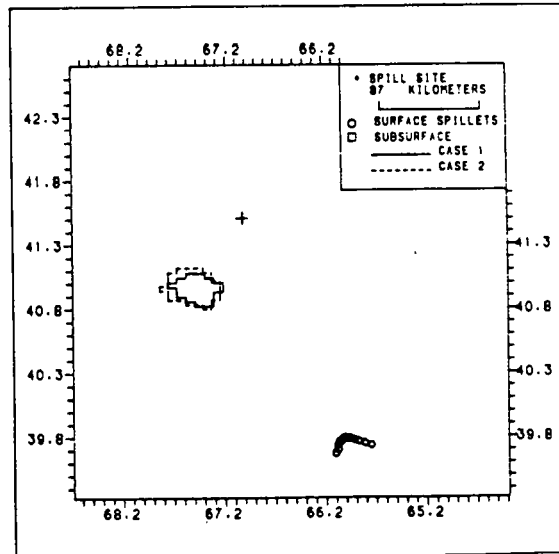
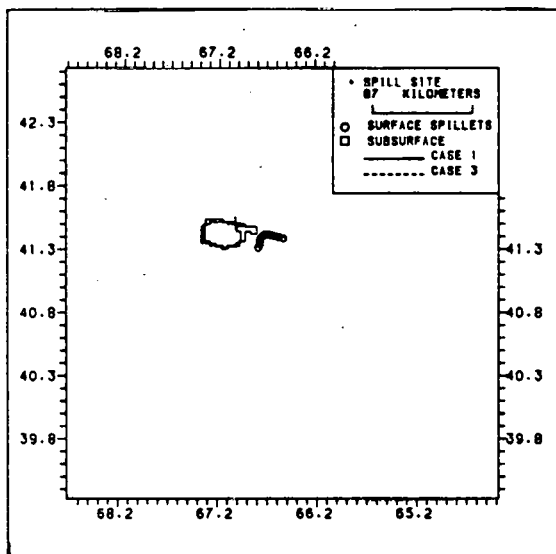
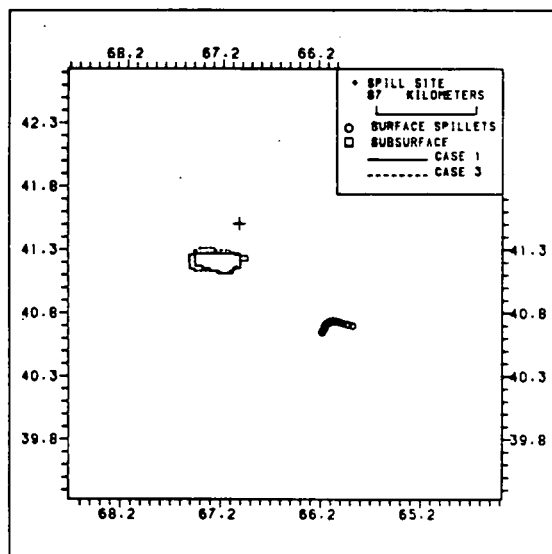


Figure 5.18 Overhead Views 100 ppb. Case 1 vs. Case 2

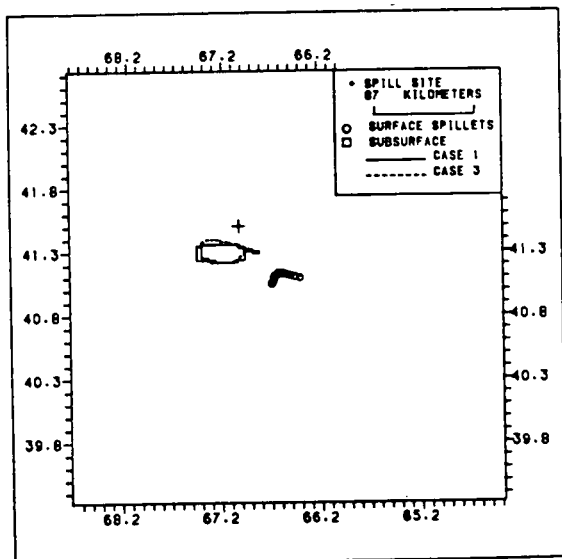
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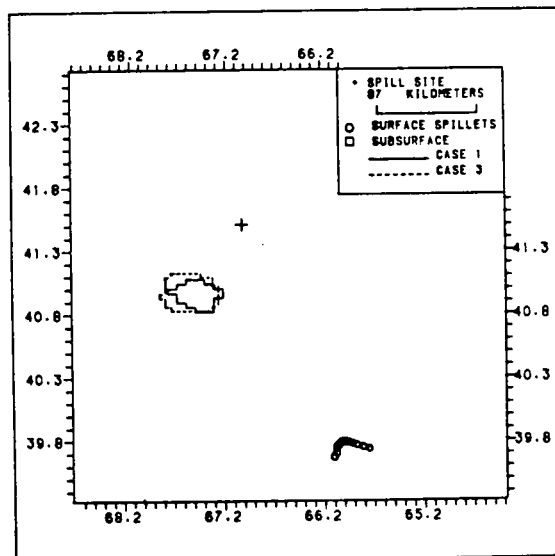
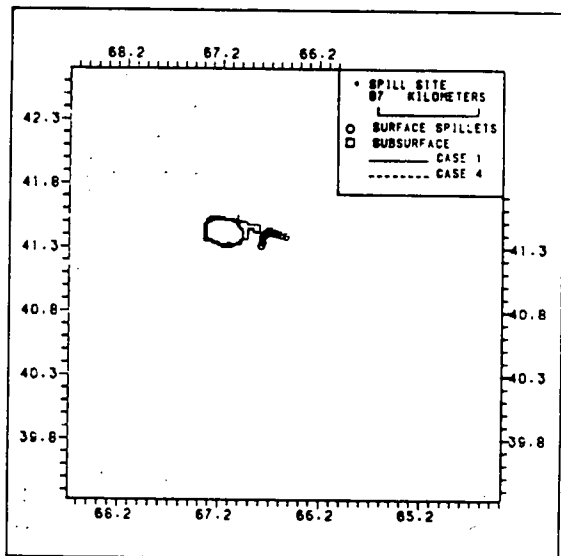
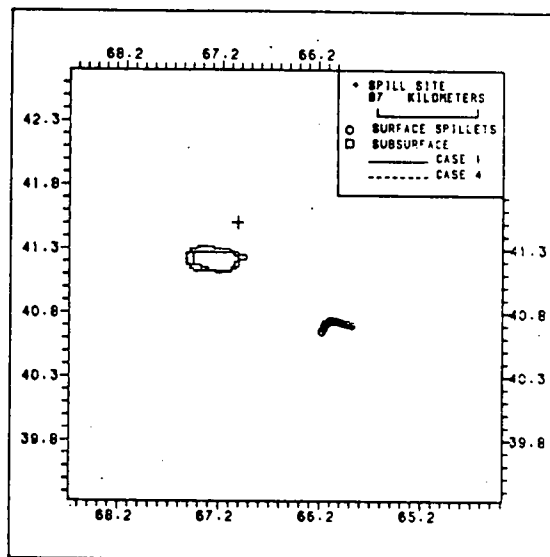


Figure 5.19 Overhead Views 100 ppb. Case 1 vs. Case 3

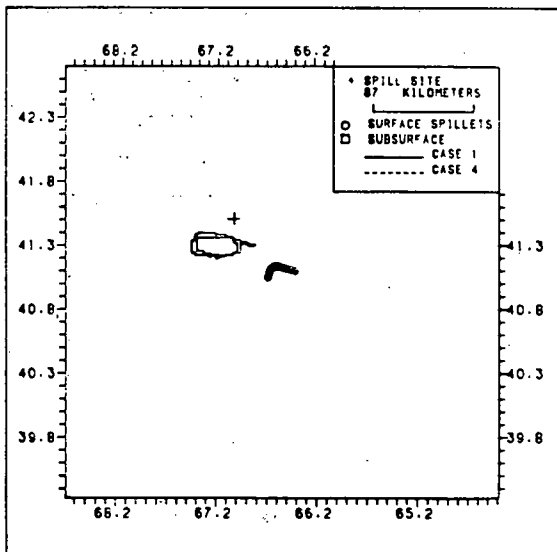
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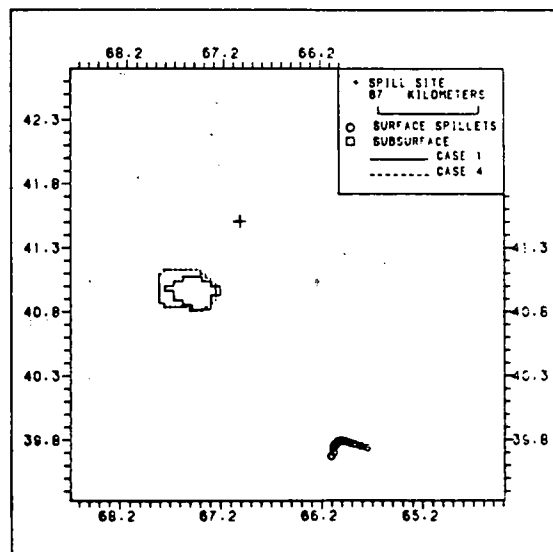
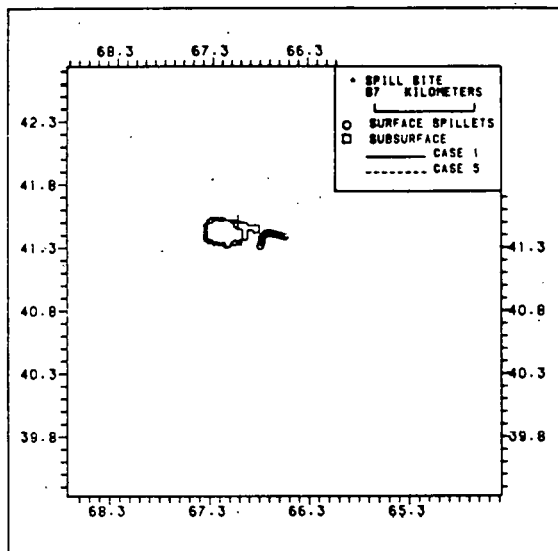
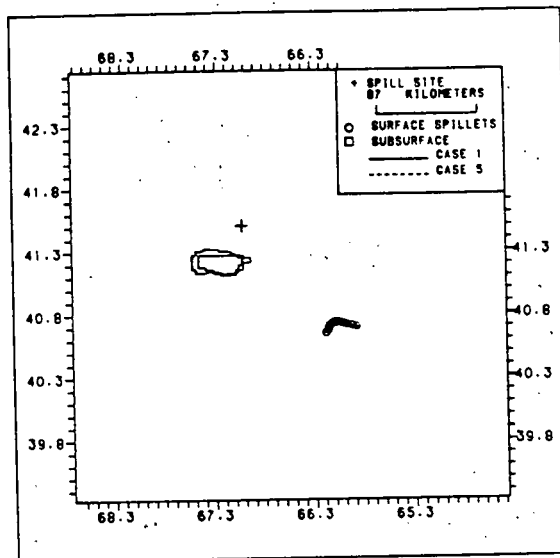


Figure 5.20 Overhead Views 100 ppb. Case 1 vs. Case 4

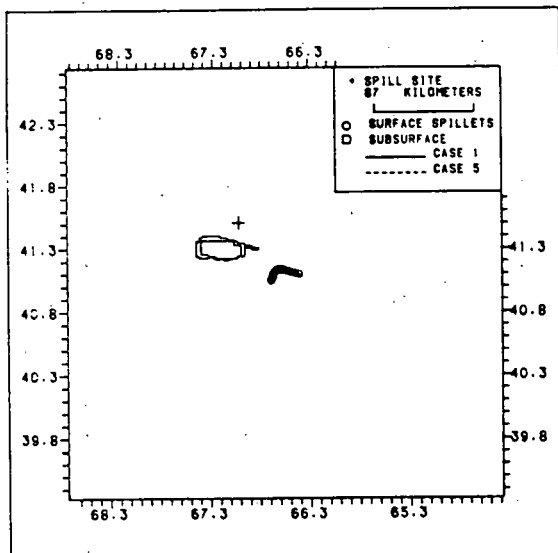
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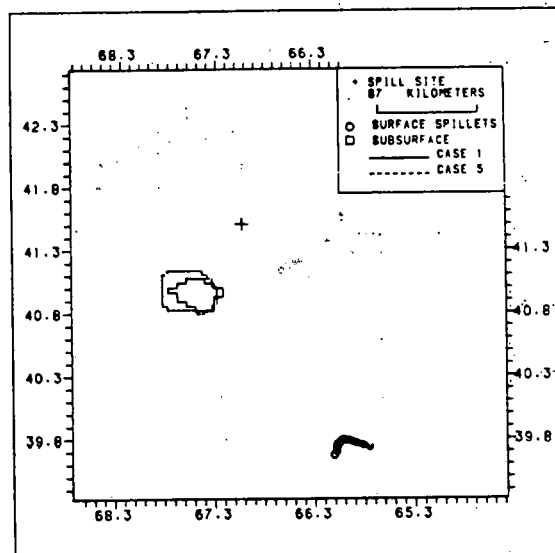
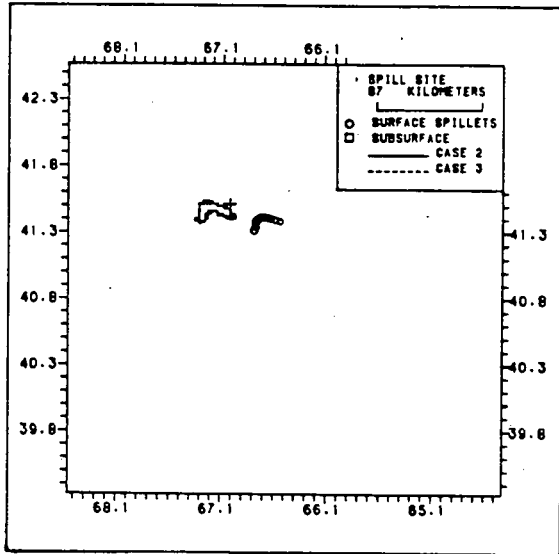
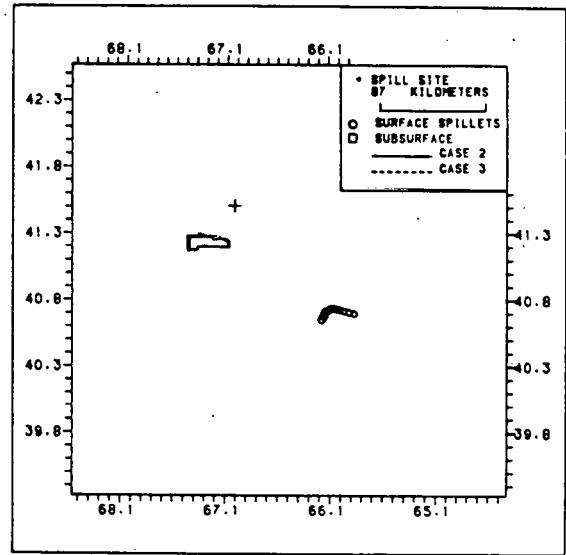


Figure 5.21 Overhead Views 100 ppb. Case 1 vs. Case 5

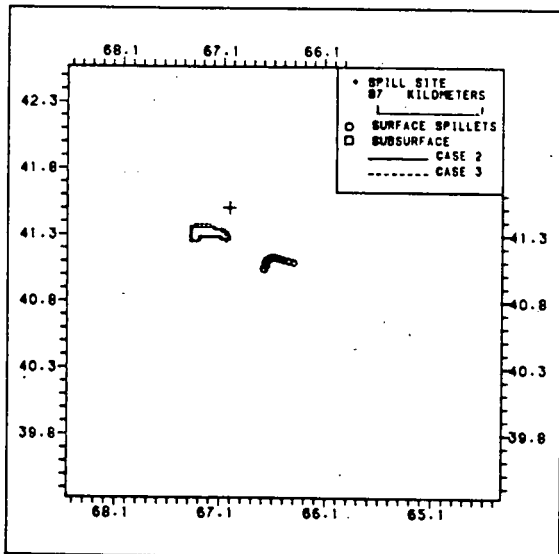
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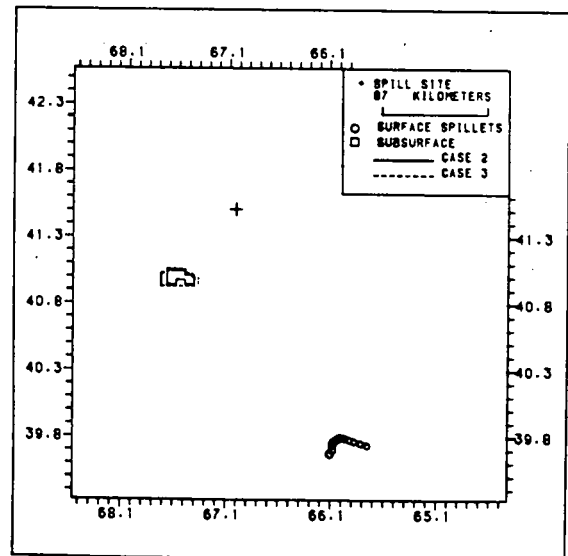
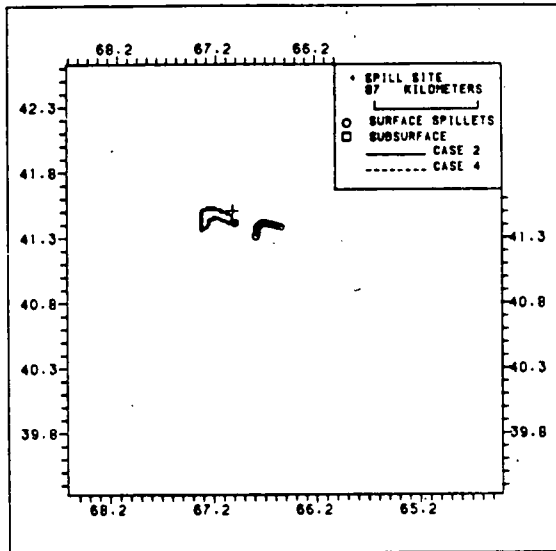
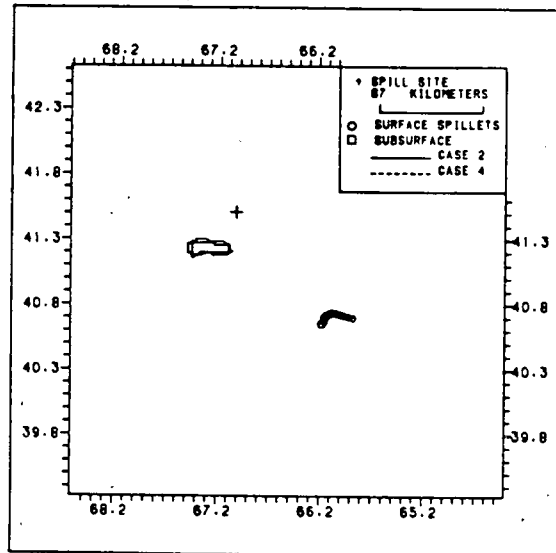


Figure 5.22 Overhead Views 1000 ppb. Case 2 vs. Case 3

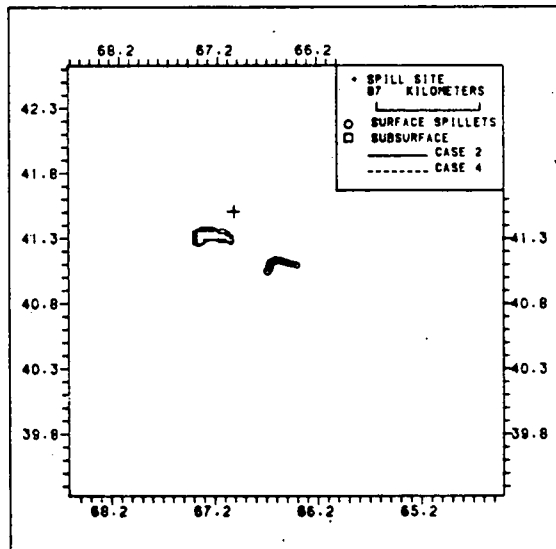
120.0 HOURS AFTER START OF THE SPILL
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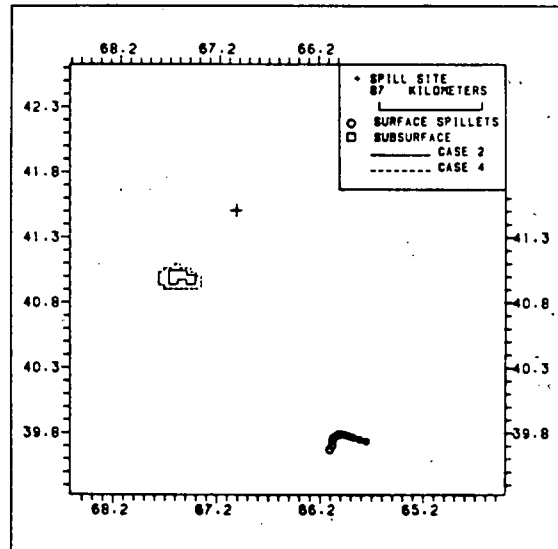
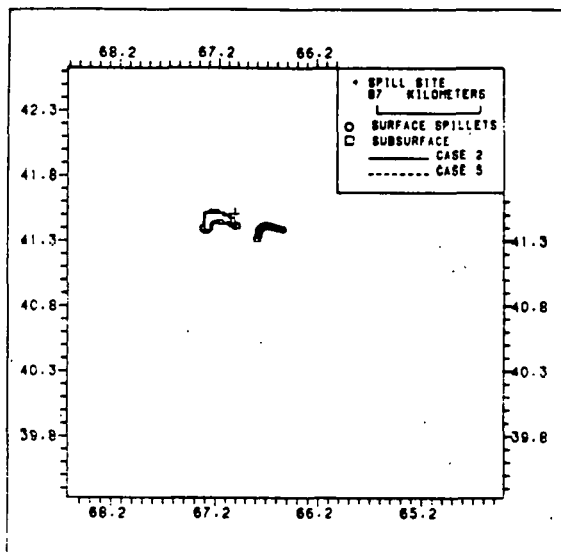
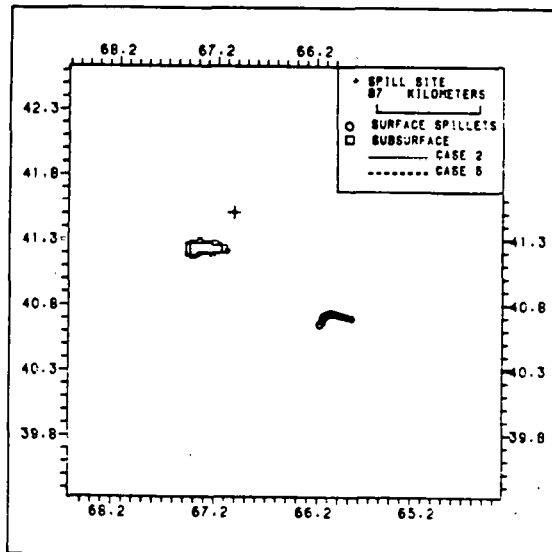


Figure 5.23 Overhead Views 1000 ppb. Case 2 vs. Case 4

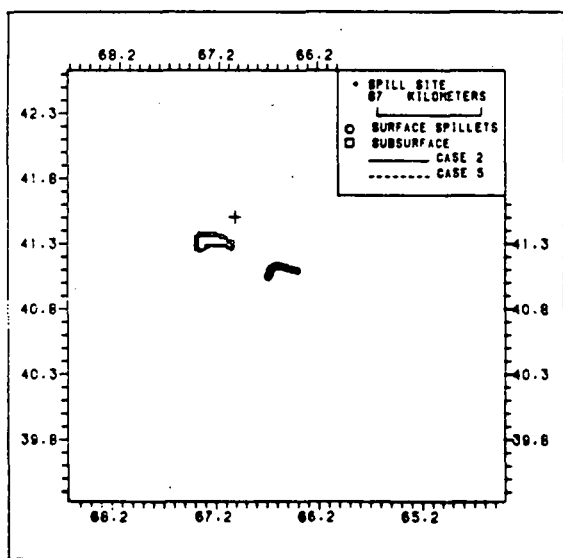
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720.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE

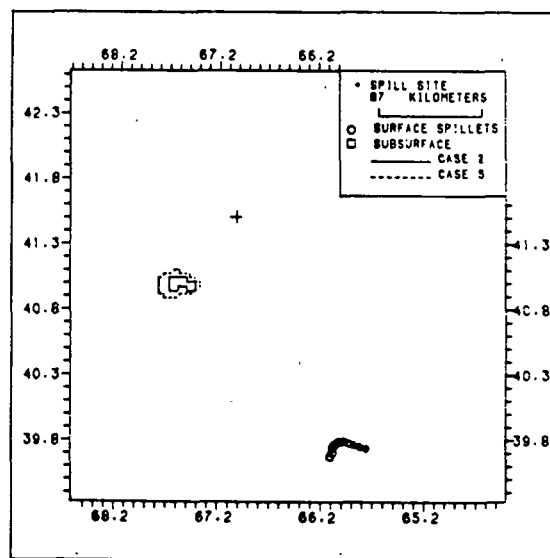


Figure 5.24 Overhead Views 1000 ppb. Case 2 vs. Case 5

The subsurface component of the spills can be compared with each other in order to determine the best strategy for the least impact on fish or fish larvae. The first aspect to consider is the timing of the treatment. In these scenarios, it can be seen that any delay in treating the spill will result in an increase in the area impacted. For coastal water scenarios, influenced to a greater extent by tidal currents, the entrained oil may return to the spill site and this aspect must be taken into consideration. The response time will most likely be even more important in this case than in the open ocean case.

The next question to consider is the percentage of oil to be dispersed. The plots of areal extent do not show the cumulative area covered but do indicate the area covered at each time step. The dispersed cases always cover more area by the end of the scenarios, but this is not true for the first 5 days for the lower concentration outlines (50 and 100 ppb). This may be of importance when toxicity is considered. The concentration for the non-dispersed case is at most one-quarter that of any of the dispersed cases. Since the spill is in a fish breeding ground, the dispersed cases are overlying the same area so the same impact will be felt for all five cases (see Figure 5.10). The higher concentration cuts, which will have more impact on the adult fish, are a result of a higher percentage dispersion (see Figure 5.13). Some larvae are thought to be affected by 50 ppb and thus lethal levels of hydrocarbon concentration may exist long after initial treatment.

It is evident from these simulated spills that local currents are of great importance as well as are the winds. Not so apparent are the effects of treatment. For example, early treatment although increasing the concentration in the water, may actually result in a smaller impacted area because of the decrease in area resulting from natural entrainment from surface spilletts. On the other hand, the lower concentrations resulting from natural entrainment in the untreated case may not impact the fisheries as much because of the lower toxicity. This complicated interplay must be investigated in greater detail in the future where such variables as response time, toxicity, etc., are varied in an in-depth application of the oil spill fishery interaction model.

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6.0 A Fishery Oil Spill Interaction Model

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Malcolm L. Spaulding

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ABSTRACT

The oil spill - fisheries impact model has been used to simulate nine variations of an oil spill scenario on Georges Bank, producing a rough sensitivity analysis of system response. Following an overview of the model system, the results and implications of these simulations are discussed along with limitations of the approach used. It is suggested that the most significant unknowns in the system are the parameters governing recruitment dynamics in the fishery, toxicity threshold values and oil entrainment rates being of secondary importance in open ocean conditions.

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6.1 INTRODUCTION

Through the National Environmental Policy Act of 1976, the United States Government has given explicit recognition to the critical importance of maintaining and restoring the quality of the environment in a manner which promotes the general social and economic welfare of present and future human generations. This research represents an actualization of the intent of this policy, employing available technological capabilities to analyze interrelationships among a number of variables in an environmental problem of contemporary significance. Typically, as many questions have been raised as have been answered, but the primary goal, the creation of a modeling methodology capable of estimating the effects of marine pollution events on biological populations, has been realized. Although the development has evolved around a specifically defined system, the conceptual approach is biologically and spatially transferrable, with each model element being sufficiently independent to permit relatively facile modification when appropriate.

The specific problem addressed here concerns the degree of impact experienced by a given stock of fish subsequent to an offshore oil spill. Recent experience on both sides of the North Atlantic Ocean has clearly demonstrated the extent to which coastal ecological resources may be damaged by large petroleum spills. In the case of the Amoco Cadiz accident off the coast of France, for example, it appears that a majority of the impacts can be assessed through direct observations. In offshore situations such as the Argo Merchant wreck, the Bravo blowout in the North Sea, or the Ixtoc I blowout in the Gulf of Mexico, the ensuing ecological consequences are far less clear. Although the oil slick disappears from the ocean surface within a few weeks after cessation of release, the full post-spill legacy is uncertain. The virtual impossibility of actually measuring these effects necessitates the application of a modeling approach.

In any modeling effort, a necessary basic decision concerns the establishment of conceptual limits on the abstraction of the real system being considered. This decision is ideally made in such a manner as to optimize the quality of the final model output, subject to the constraints imposed on the project. Allotted model development time, financial support limitations, and the existence and availability of appropriate data are the most important of these constraining factors, and all came to bear on the definition of the model system selected here.

The initial intent in the present case was to estimate the environmental impact of oil spills at sea, and the effect on this impact of chemically treating a spill. The most objective measure of impact is one with final dimensions of dollars and cents, dictating that commercially exploited species be included in an explicit manner. Thus the cost of a spill under a variety of different treatment scenarios could be investigated, the quality of the model's output being evaluated according to the level of confidence associated with its predictions.

Although a reliable whole-ecosystems impact model may eventually be achievable, a review of related efforts (Reed et al., 1978), and an evaluation of currently available biological baseline data strongly suggested that pursuit of such a model in the time frame and funding level of this

project task would be at the expense of output quality. The single species fishery model, a relatively well established art form supported by a healthy literature dating generally from the work of Verhulst in the nineteenth century and more specifically from Barenov's (1918) application of first order kinetics to a fish population, was selected as the simplest viable subset of the ecosystem approach. It was felt that sufficient uncertainties were evident in the problem without the addition of further conjectures and postulates regarding rates and processes of species interactions. The application of Okham's razor (see Hutchinson, 1978) in this case requires the identification of a position between employing too many parameters to justify from the adequacy of the data base, and too few to do justice to the system. Thus in adopting the principle of parsimony of parameters, permitting a tractable entry into the complexities of the problem, the advice of Lagrange is observed: seek simplicity, but distrust it. The potential magnification in complexity thus avoided is demonstrated in a paper by Andersen et al. (1977) describing a multispecies fishery model in which the simulation of 12 interacting species required the input of some 1600 separate parameters.

The selection of a physical area for the initial model application was relatively straightforward, since Georges Bank (Fig. 6.1), which has supported a thriving fishery for over a century, has recently become the focus of offshore continental shelf hydrocarbon exploration interests. The oil spill fishery interaction problem in this area is therefore potentially very real. Selection of the cod stock on the Bank followed from the data considerations discussed above, as well as the abundance of biological and modeling literature on the species. The previous reference further details this information.

6.2 MODEL OVERVIEW

Because the model has been described in detail elsewhere (Reed et al., 1978, 1979a, 1979b) only a brief overview will be given here. The system is composed of three major interacting components: a fishery sector, an ocean transport sector, and an oil spill fates sector, as described below.

6.2.1 Fishery Model

As shown in Fig. 6.2, the population model cycles on a daily timestep when operating in conjunction with other system components. When operating alone, this timestep can be increased up to five days with little decrease in numerical accuracy, reducing computer time proportionately. The adult fishery model is constructed along well established lines (e.g. Beverton and Holt, 1957; Walters, 1969), whereas the egg and larval stages have been modeled using techniques drawn from other areas of mathematical ecology (Lotka, 1925; Pielou, 1969). The structure of the fishery model is shown schematically in Fig. 6.3.

The model has 17 adult age classes, enough to include all fish sampled in recent surveys (Heyerdahl et al, 1976). They increase in length and weight according to a published growth equation (Pentilla et al, 1976) for the Georges Bank stock. The i th adult age-class is

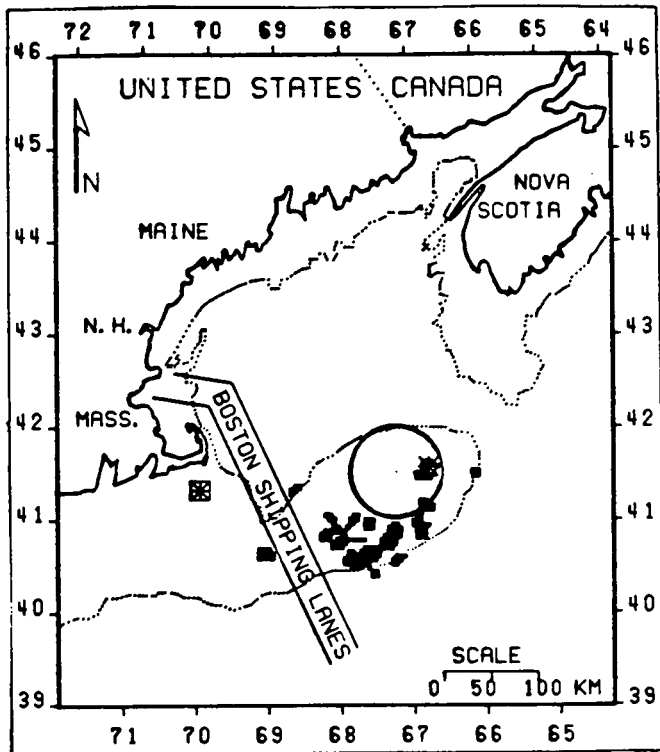


Figure 6.1 Map of Georges Bank, showing the 100 meter bathymetric contour, the spawning area (circle), oil exploration tracts (dark regions), commercial shipping lanes, wind data source (■), and the location of the simulated oil spill (⊗).

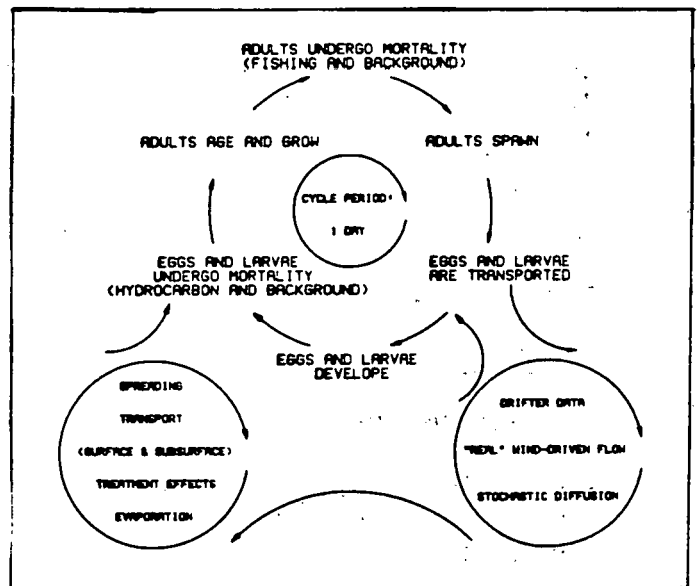


Figure 6.2 Model System Cycles, showing processes simulated in each sector. Arrows indicate information flow.

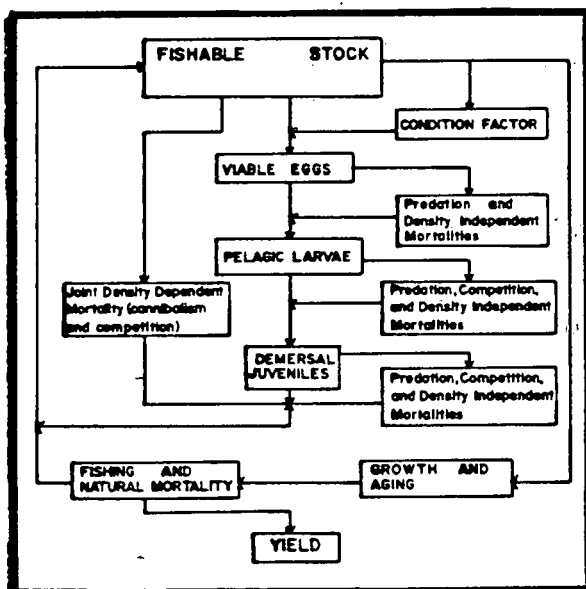


Figure 6.3 Process schematic for the fishery population model.

subject to a mortality equation following first order kinetics,

$$dN_i/dt = -(M_i + F_i)N_i, \quad (1)$$

in which M_i and F_i are natural and fishing mortality coefficients respectively, the former including all types not induced by the latter. Fishing mortality is assumed linearly proportional to standardized fishing efforts:

$$F_i = q S_i E(t) \quad (2)$$

Q is a species and stock dependent catchability coefficient (Gulland, 1977), S_i is net mesh selectivity for the i th age-class, and $E(t)$ is a measure of the fishing effort exerted on the stock during the time interval t .

The fecundity of cod appears well correlated with weight, although, as with all such characteristics, the relationship varies from one stock to another (Daan, 1973); Garrod, 1977; Bigelow et al., 1953; Nikolskii, 1965; Gulland, 1964). This literature suggests a value of 200 to 250 eggs per gram female, which conforms reasonably well to an estimate by Bigelow, et. al. of one million eggs per average female, although falling somewhat short of their estimated maximum of nine million.

Temporal distribution of spawning cod on Georges Bank remains something of an enigma, it being uncertain whether cod spawning activity is triggered by day length, temperature, or other environmental factors (F. Serchuck, National Marine Fisheries Service, Woods Hole, personal communication; Wise, 1961). Bigelow et al. (1953), Colton et al. (1977, 1978), and Walford (1938), support the observation that spawning occurs with varying degrees of intensity from November to late April, with a maximum occurring in March and a second smaller peak in the late Fall.

The model takes on spatial dimensions through the simulation of this activity. On any given day of the year, a percentage of the females of each sexually mature age class are assumed to release their eggs. (The fact that not all will be properly fertilized is accounted for in the density independent mortality parameter M_1 in Equation 3. Possible relations between age and time of spawning are not included). The total number of eggs available for spawning on that day is divided into a set number of groups, or sub-cohorts. Thus each particle in the transport model represents one sub-cohort of organisms in the population model. As simulated time progresses, each particle is transported, and represents a diminishing number of developing eggs, larvae, or post-larvae. When a sub-cohort reaches the demersal stage, it loses its explicit representation in space, while of course retaining its presence in the population model.

The major uncertainties in the biological sector of the model exist in the egg and larval mortality representations. These are formulated to require as few arbitrary parameters as possible, while simulating these stages in sufficient theoretical detail to resolve toxic effects which vary in magnitude from one developmental stage to the next. There are five first year stages represented in the model. These are an egg stage

(E), three planktonic larval and postlarval stages (L), and a demersal juvenile stage (J). The equations governing mortality during these various developmental periods are:

$$dE/dt = (M_1 + M_2 * E) * E, \quad (3)$$

$$dL/dt = (M_3 + M_4 * L) * L, \text{ and} \quad (4)$$

$$dJ/dt = (M_5 + M_6 * J + M_7 * \sum_{i=1}^{17} N_i * P_i) * J. \quad (5)$$

Equations (3) and (4) each include a density dependent and a density independent mortality term, whereas Equation (5) incorporates a set of adult-juvenile interaction terms as well. The theory upon which these equations are based derives from Lotka (1925), who employed the concept of a Taylor expansion about some hypothetical equilibrium value. Density dependent mortality of an intragroup nature, as associated with parameters M_1 , M_4 , and M_6 , is intended to represent competition among individuals of the group for limited resources (e.g. food), or mortality due to predation by some species external to the explicit model formulations (e.g. herring). Density dependence between groups may result from competition for shared resources, or a parasitic (e.g. cannibalistic) relation. There is considerable evidence of cannibalism among Gadoids (see for example Daan, 1973, or Bigelow et al., 1953), and is a theoretically acceptable explanation for population control in Gadoids (Cushing et al., 1977). The third term in Equation (5) is designed to simulate this fact, the P_i being age-specific predation rates. Recent evidence reported by Ellertsen et al. (1979a) indicates that cannibalism amongst larval and postlarval Gadoids may contribute significantly to mortality, perhaps outweighing effects of food density. This process is not yet explicitly incorporated here. (Further discussion of these equations, their derivations, and an algorithm for the numerical solution of Equation (5) may be found in Reed and Spaulding, 1978.)

Sensitivity to the toxic action of hydrocarbons appears to result from a complex interaction among several variables (Malins, 1977):

- (1) chemical composition of the oil,
- (2) duration of exposure,
- (3) concentration of soluble aromatics in the water,
- (4) stage of development of the organism,
- (5) physical condition of the organism, and
- (6) species.

Along the same lines as suggested by Andersen et al. (1977), efforts have been made to utilize published bioassay data (Kunhold, 1970, 1977; Wilson, 1977) to partition density independent mortality parameters of cod during planktonic stages (Reed and Spaulding, 1978). Although the model is designed to keep account of the variables relevant to toxicity, difficulties of interpretation as well as uncertainty levels elsewhere in the system (e.g. oil entrainment rates, details of ocean transport estimates) have prompted the adoption of a threshold assumption: any eggs or larvae entering an area in which the concentration exceeds their respective threshold values are deleted from the system. In light of the

fact that the presence of hydrocarbons in the water will adversely affect the food supply (Wolfe, 1977, Workshop...., (1975) as well as the larvae themselves, this appears reasonable, erring perhaps marginally on the environmentally conservative side.

Development during the first year is modeled in five stages: eggs, yolk-sac larvae, larvae adapting to free-feeding, adapted free-feeders, and bottom-dwelling juveniles. These stages were selected as those between which definite differences in susceptibility to hydrocarbon toxicity have been observed by Kunhold and Wilson. Egg hatching rates are well represented by a negative exponential curve, probably reflecting temperature dependent chemical interaction rates in egg development. Yolk-sac resorption requires from 4 to 12 days (Wise, 1961; Bigelow et al., 1953). Work being performed by Ellertsen et al. (1979b) suggests that food density may be significant in determining the duration of this stage, but for lack of any deterministic relation, eight days is used here. The larvae must then adapt to catching planktonic organisms, primarily copepod nauplii. Kunhold found the larvae most susceptible to hydrocarbon toxicity during this stage. According to Cushing et al. (1977), the Norwegian investigator H. Dannevig grew cod larvae from hatching to metamorphosis in 70 days, and it is believed that they seek bottom about a month later. These development rates are certainly variable with such things as temperature and food availability, but except for hatching rates, constant values have been used in the model due to lack of hard data.

Pre-recruit mortality parameters are notoriously difficult to evaluate, since what few values exist are usually derived from laboratory observations and do not reflect conditions in the open ocean. It is nonetheless desirable to use whatever our best estimates may be, to reduce the need for blind 'model tuning' in the final stages. Thus a value equivalent to 60% mortality has been used for the density independent rate for eggs (Laurence et al., 1976), and it is hypothesized that demersal juveniles die of natural causes (e.g. disease or starvation) at about twice the rate of the adults. The four remaining density dependent parameters were assigned values resulting from a series of steepest descent searches (Walters, 1969) using the sum of the squared differences between the modeled and the observed annual yields from 1932 to 1952. Several approximately equivalent local minima were found. Of these, most were rejected for biological reasons, such as the improbability of having 90% survival to the demersal stage. Of the remaining sets of mortality parameters which appeared acceptable from the modeling point of view, three were selected for further investigations. As shown in Fig. 6.4, these bracket the likely range of first year mortality curves.

Figure 6.5 shows a comparison of model behavior when operating under the first year mortality curves of Fig. 6.4. In each case, the model is initiated with an equilibrium population, and a perturbation is introduced by assuming the complete failure of the subsequent yearclass. It can be seen that the modeled stock fluctuations increase both in magnitude and duration as density dependent mortality emphasis shifts from intra-egg and intra-larval stages (Mode 1) to the adult-juvenile formulations (Mode 3). This behavior corresponds conceptually to a decreasing negative slope on the stock-recruit curve at the replacement point, as discussed by Allen et al. (1974). The biological explanation

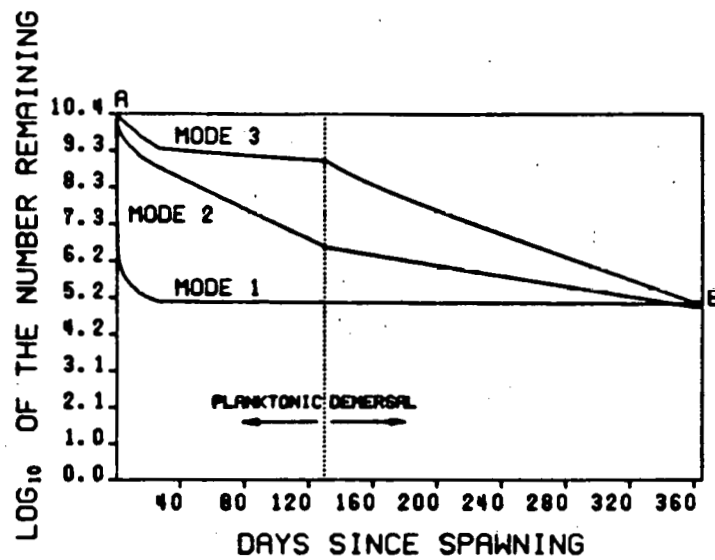


Figure 6.4 Three piecewise-continuous mortality curves for the first year of life. The curves result from three different sets of parameters in Equations 3, 4, and 5.

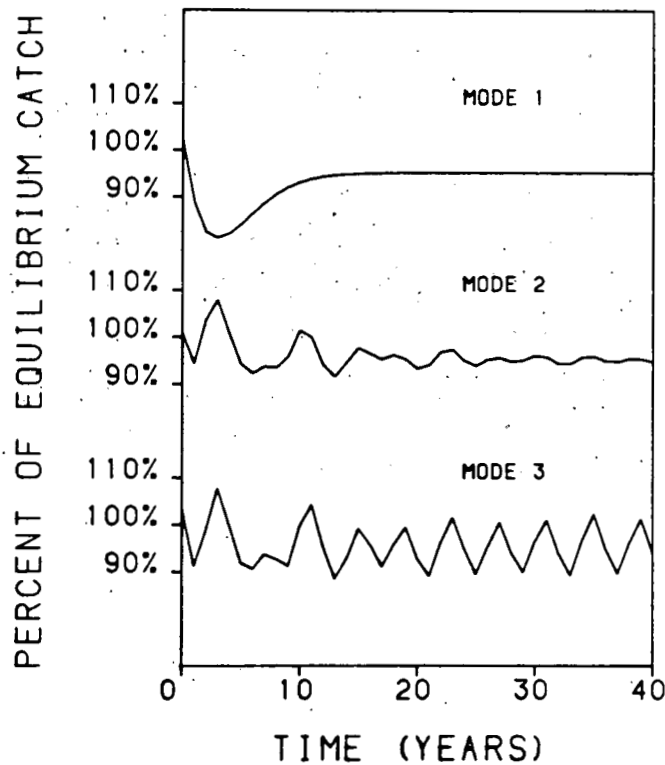


Figure 6.5 Comparison of modeled response to an arbitrary perturbation under the three nodes of Figure 4.

lies in the fact that increasing the relative importance of the adult juvenile interaction such that cannibalism (or resource competition) is the dominant controlling factor for population size causes the direct transference of oscillations in the parent stock to oscillations of the opposite sign in the associated O-Group. If the relationship becomes strong enough, the model becomes unstable.

Although the average error of the predicted yield is on the order of 20% of the average catch (Fig. 6.6), the model demonstrates a reasonable ability to follow the trends in the record ($r=0.81$). The model does not predict catch size with great accuracy, but the impact estimates required here will be the differences between predicted catches with and without a spill. While the actual predictions may be off by 20% or more, to the extent that the model follows the yield trends, these differences may only be in error by a few percent. The relative impact estimates themselves may be more accurate than the absolute yield estimates from which they derive.

6.2.2 The Ocean Transport Model

The marine transport model consists of three superimposed flow processes, each representing transport energy spanning a different portion of the energy spectrum. Although such separation neglects nonlinearities in the real system, this approach is adopted in lieu of a two or three dimensional numerical modeling effort involving the solution of the Navier-Stokes equations on a phase-space grid of sufficiently fine mesh to resolve the processes of interest. The available data base for verifications of larval fish distributions hardly warrants the time and effort necessary to produce such a model. The methods described here are on a level of approximation consistent with others in the physical sector of the model (e.g. spawning rates and locations), and appear to yield useful and credible transport estimates, as discussed below.

The low frequency seasonal circulation patterns have been deduced from oceanic drifter data gathered over approximately a decade (Bumpus et al., 1965). The resulting flow fields supply estimates of net transports on temporal scales of weeks and months, arising as the residual of tidal, meteorological, and river inflow events, as well as pressure forcing on the ocean boundaries of the modeled area. A triangular grid was constructed covering the area of interest (Fig. 6.7), and velocity components were assigned at each node. Linear interpolation is performed between seasonally adjacent data sets to supply smoothed daily input to the model. Advective velocities at a given point within a grid element are assigned by fitting a plane through the component values at each of the three surrounding nodes, thus spatially interpolating values at any internal point.

Intermediate frequencies of transport energy are input through wind forcing on time scales of a few hours to several days. Decoupling of this input from the long-term effects, it probably imparts to the real systems (Csanady, 1976) is achieved by first passing a digitized record of wind data for the time period of interest through a high pass filter with a corner frequency of one cycle every ten days. In this way, only energy associated with trends occurring over time periods less than ten days is retained in the record. This filtered wind record is then used as input to a simple two-dimensional model of the wind-driven surface

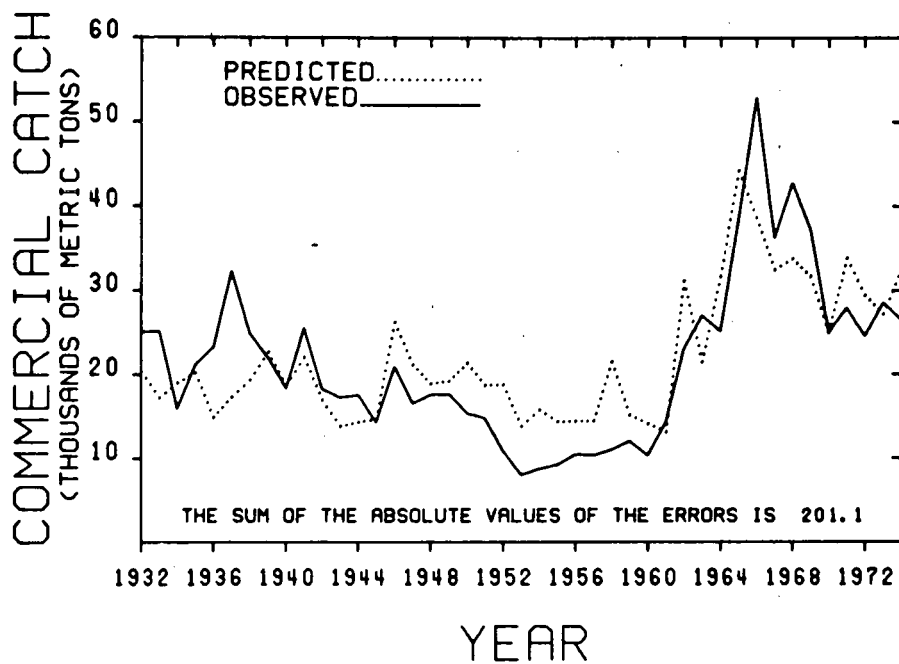


Figure 6.6 Modeled versus observed catch for Georges Bank cod.

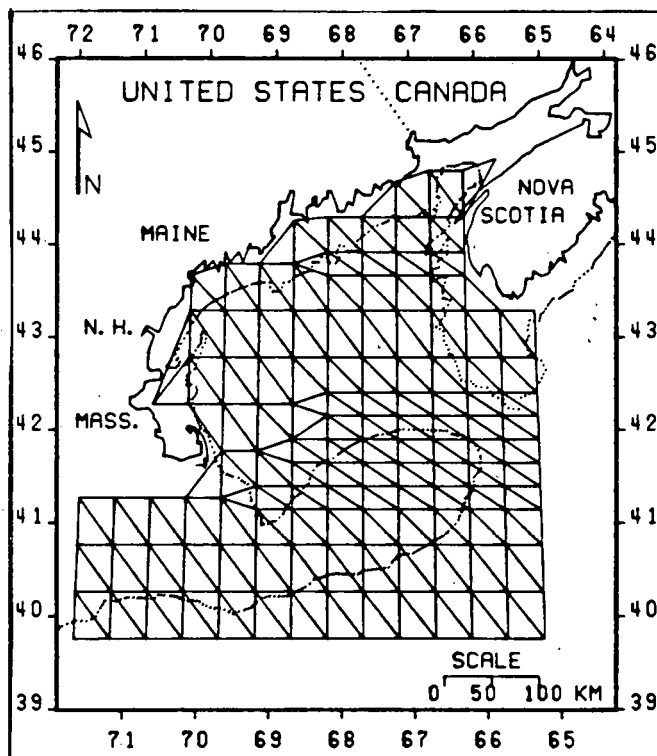


Figure 6.7 Triangular grid system for the ocean transport model.

layer. Because it does not appear elsewhere, the description of this sector of the model will be relatively detailed.

The complete Navier-Stokes equations describing the motion of an incompressible fluid continuum may be averaged over H , the depth of the wind-driven layer. Because the area being modeled (Georges Bank) is far from any land boundaries, and because this wind driven depth will in general be small relative to the total depth, so that for coherent forcing periods below a few days only small return flows in the lower depths will be required to eliminate surface setup, the pressure gradient terms can be neglected. If the depth H is assumed constant for the duration of at least one sampling interval in the wind record (here three hours), then the convective acceleration terms can also be dropped from the equations. The usual quadratic forms of the wind stress terms can be replaced by linear approximations to preserve the validity of superposition. Data analyzed and reported by Kirwan et al. (1979) suggests that a linear law relating wind to wind drift current may be as good as the quadratic formulation for long terms (>5 days) estimates. Thus the wind stress at the surface in the x direction (positive to the east) is

$$\tau_x = \rho_a R_S U \quad (6)$$

and in the y direction (positive north) is

$$\tau_y = \rho_a R_S V \quad (7)$$

in which ρ_a is the air density, U and V are the wind velocities in the x and y (east and north) directions respectively, and R_S is an empirically derived constant. If a hypothetical stress at the bottom of the wind driven layer is similarly linearized, the equations of motion become

$$\frac{du}{dt} = fv + \frac{\rho_a R_S U}{\rho_w H} - \frac{R_H u}{H} \quad (8)$$

$$\frac{dv}{dt} = -fu + \frac{\rho_a R_S V}{\rho_w H} - \frac{R_H v}{H} \quad (9)$$

In Equations 8 and 9, U and V are the eastward and northward ocean current velocities averaged over the wind driven depth H , f is the Coriolis parameter, R_H is the linear stress coefficient at the depth H , and ρ_w is the density of sea water. Assuming the depth H to be constant over one sampling interval in the wind time record, this set of coupled ordinary differential equations has the simple solution.

$$u(t) = e^{-\left(\frac{R_H}{H}\right)t} \left[(u_0 - u_\infty) \cos(ft) + (v_0 - v_\infty) \sin(ft) \right] \quad (10)$$

$$v(t) = e^{-\left(\frac{R_H}{H}\right)t} \left[(v_0 - v_\infty) \cos(ft) + (u_0 - u_\infty) \sin(ft) \right] \quad (11)$$

wherein u and v are the orthogonal currents at the beginning of the time interval, and the asymptotic velocities for large times t are given by

$$u_\infty = \frac{\rho_a R_S}{\rho_w} \left[\frac{R_H U + HfV}{R_H^2 + H^2 f^2} \right] \quad (12)$$

$$v_\infty = \frac{\rho_a R_S}{\rho_w} \left[\frac{R_H V - HfU}{R_H^2 + H^2 f^2} \right] \quad (13)$$

Equations 10 and 11 describe circular motion with damping and an off-set. The angle of the net transport to the right of the wind can be most easily calculated by aligning the axes such that $U=0$, giving

$$\theta = \pi/2 - \arctan \left[R_H/Hf \right] \quad (14)$$

from which it can be seen that the transport will be 90 degrees to the right of the wind for zero bottom stress or infinite depth, in agreement with Ekman's classical analysis.

In reality, the mixed layer depth will be a function of wind speed and duration, sea state, and density stratification (Phillips, 1977; Liebovich, 1977; Kullenberg, 1976; Niiler, 1977). As pointed out by Gonella (1971) and Csanady (1972), the correct formulation for H as a function of time in very deep water would eliminate the necessity of the "interlayer stress" artifice (second term on the RHS of Equations 8 and 9). The resistance to surface stress in deep waters arises from a downward flux of momentum and internal dissipation, so the correct lower boundary condition is zero stress at the (variable) depth H . Because of the lack of agreement on vertical eddy viscosity formulations for the solution of this problem (see for example Huang, 1979), an arbitrary depth of 10 meters for a 3 hour response time has been selected as suggested by the literature overview summarized in Table 6.1. This depth includes the majority of cod eggs and larvae in the area, and unless oil actually sinks, it appears doubtful that any significant amount will penetrate deeper than this (McAuliffe, 1977).

Observer	Drift Layer Depth (meters)	Depth Averaged Current (as Percent of Wind Speed @ 10 m.)	Approx. Establish. Time (hrs)	Drift Angle (to the rt. of W)	Comments
Nansen (1902)	-	~ 1%	-	20-40°	observations of icebergs
Ekman (1905)	~ 50	1.3%/sin ^{1/2} ϕ	~10-20	90°	theory
Smith (1931)	~ 20 ~ 5	< 1% ~ 1%	- -	40° 20°	deep immersing iceberg small iceberg
Csanady (1972)	9-18	2%	1-3	-10-60°	Lake Huron observations
Csanady (1974)	10-20	-	3-8	-	theory
Murray (1974)	10	2%	3	10-90°	near shore, shallow
Mellor et al (1975)	25	-	16	-	model compared w/ data
Niiler et al (1977)	10	-	1-2	-	theory and observation
Csanady (1976)	16	-	-	-	theory and observation
Gonella (1971)	10-15	1%	2-3	-	theory and observation
Madsen (1977)	25	1%	~ 3	10°	modeled
Kondo et al (1979)	20	~ 1%	16	17°	observed and modeled
Kirwan et al (1979)	surface	-	-	15°	theory and observation

Table 6.1: Summary of Literature Estimates of Wind-Driven Flow Parameters

The most widely accepted formulation for the wind stress, supported by a large number of laboratory and field investigations, is a proportionality with the square of the wind speed multiplied by the density of the air. This is consistent with dimensional considerations, and corresponds to drag formulations for fluid flow around a solid body. One possible method of assigning a value to the parameter R_S would be to equate the energy input from atmosphere to ocean in the linear model with that prevailing under the quadratic stress formulation. This was not done because it would have amounted to forcing energy from lower frequencies into the domain of the filter applied to the wind record.

The problem has instead been approached in a simple statistical manner. An estimate of R_S in terms of the "correct" quadratic formulation,

$$\vec{\tau}_q = \rho_a C_d \left| \vec{W} \right| \vec{W} \quad (15)$$

results from a comparison with the linear expression

$$\vec{\tau}_l = \rho_a R_S \vec{W} \quad (16)$$

Equations 15 and 16 suggest that R_S , with dimensions of velocity, may be taken as a measure of the mean background wind velocity magnitude, and should, therefore, be derived explicitly for each specific wind record employed. The filtered wind record used here spans from September 1972 to September 1973, and has maximum and minimum magnitudes of 16.4 and 0.114 meters/sec. with a mean of 5.1 meters/sec. Using $C_d = 0.002$ (see for example Wilson, 1960, or Wu, 1969), this gives a value of $R = 0.01$ meters/sec.

Winant et al. (1979) statistically compared quadratic and linear formulations for the bottom stress in water depths of 30 to 40 meters, and were unable to determine which parameterization was more accurate, lending further support for the linearization imposed here. Their parameter estimates for R_H , varying from 0.04 to 0.2, are derived on the assumption that surface and bottom stress components are equal (i.e. at steady state conditions) and appear high. A second estimate of R_H can be determined by estimating the asymptotic magnitude of the depth averaged current as a function of wind speed from the literature (Table 6.1), and solving Equations 12 and 13 for R_H . Using $R_S = 0.01$ meters/sec., a density ratio of 0.00125, a depth of 10 meters, $f = 0.000097$ radians/sec, and solving the relation

$$(u_\infty^2 + v_\infty^2)^{\frac{1}{2}} = 0.01(U^2 + V^2)^{\frac{1}{2}} \quad (17)$$

by substituting for u_∞ and v_∞ from Equations 12 and 13 gives $R_H = 0.001$. These values imply an asymptotic drift transport angle of 44 degrees to the right of the wind, attained within $\pm 2\%$ after 7 hours.

The behavior of the model for other values of the parameters is shown in Figs. 6.8-10. Empirical validation of such a model is necessarily subjective, not only because vertically uniform slab flow is an extreme simplification of actual wind-driven ocean current profiles, but also

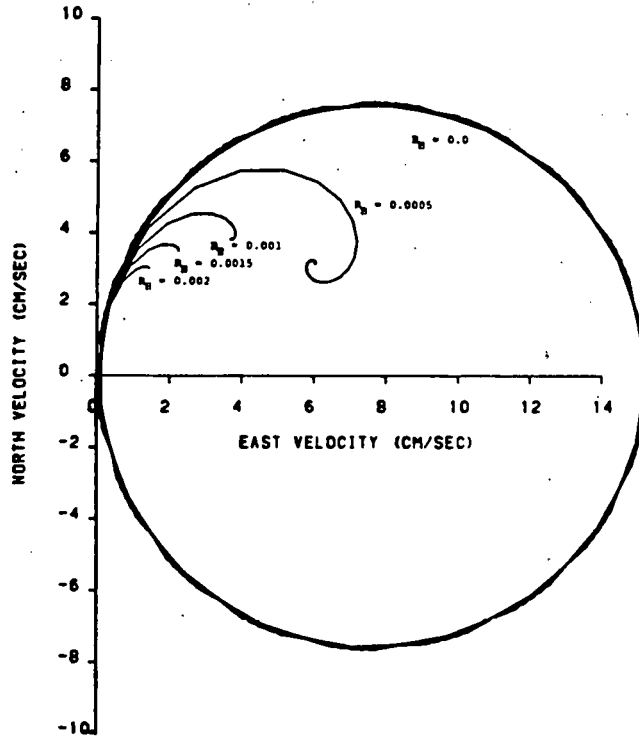


Figure 6.8 Response of the wind drift equations (Equations 10 and 11) for several values of the linearized interlayer stress R_H .

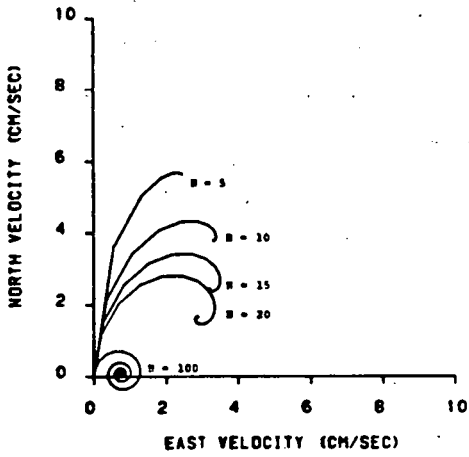


Figure 6.9 Response of Equations 10 and 11 for various drift layer depths (meters).

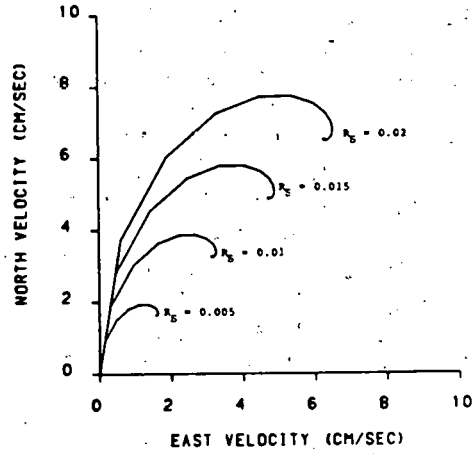


Figure 6.10 Response of Equations 10 and 11 for several values of the linearized surface stress coefficient R_S (in/sec).

because documented observations of atmosphere-ocean momentum interactions are themselves so variable. The studies summarized in Table 6.1 suggest that, for an establishment time of 3 hours, plausible attributes of the wind drift current are a depth of 10 meters, a vertically averaged speed of 0.1% that of the wind, and a drift angle of 20 to 60 degrees. If the observations by Smith (1931) of drifting icebergs can be taken as reflecting vertically averaged drift angles and speeds, then 30 degrees might be a reasonable intermediate value. For the parameter values used here ($r_s = 0.01$ m/sec; $R_H = 0.001$ m/sec; $H = 10$ meters) the linear model predicts a drift angle about 30 degrees to the right of the wind after 3 hours, and a speed 0.1% that of the wind.

The third transport process in the model is dispersion, assumed to result from energy input at frequencies greater than and equal to that of the tides, as well as energy cascaded into this frequency range through dissipation processes in the real system. Dispersion is modeled as a random walk process occurring with a mean velocity magnitude

$$V = \sqrt{6D/dt}, \quad (18)$$

(see Appendix A), in which dt is the simulation timestep, and D is the diffusivity, taken from an oceanic diffusion diagram (Okubo, 1974).

In summary, the transport of ichthyoplankton and entrained oil is simulated through the juxtaposition of a random walk diffusion process, a wind-driven velocity component responding to an actual time series pre-processed through a high pass filter, and a drifter-inferred seasonally varying aspect.

Validation of the fishery cum ocean transport model has been described in the references already cited, but is discussed briefly here to clarify the significance of results, and to emphasize the importance of longterm methodical data acquisition programs to the success of ecological impact modeling endeavors. The basis for the validation methodology proposed here is a space-time history of larval fish concentration data. Unfortunately, such data is extremely expensive to acquire, and National Marine Fisheries Service data for larval cod on Georges Bank exists only for December and February, so that spring verification is not possible. (A data set for March, 1976 may soon become available.) The length of the record (four years) is insufficient to warrant actual statistical comparison of model results with the data. Qualitative comparisons (Figs. 6.11-14) suggest that the model performs reasonably well. If the data record were longer, an average distribution with variance could be derived, and a confidence interval could be placed on the model predictions. In addition, one could begin to consider the environmental factors relating to specific distributions, thus revealing which of these factors when included in the model would most improve performance.

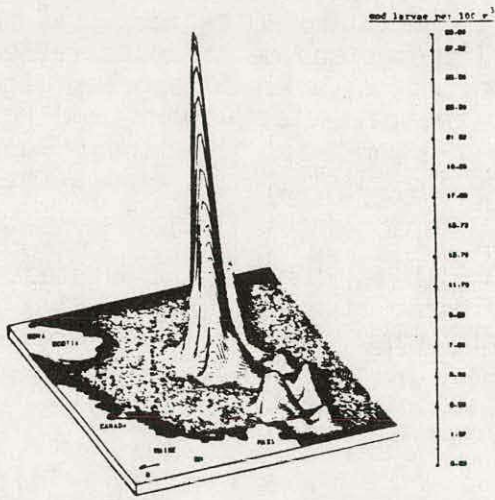


Figure 6.11 Observed Larval cod distribution for December, 1974. The larvae southeast of Massachusetts are associated with the Southern New England Cod Stock (Wise, 1963) not modeled here.

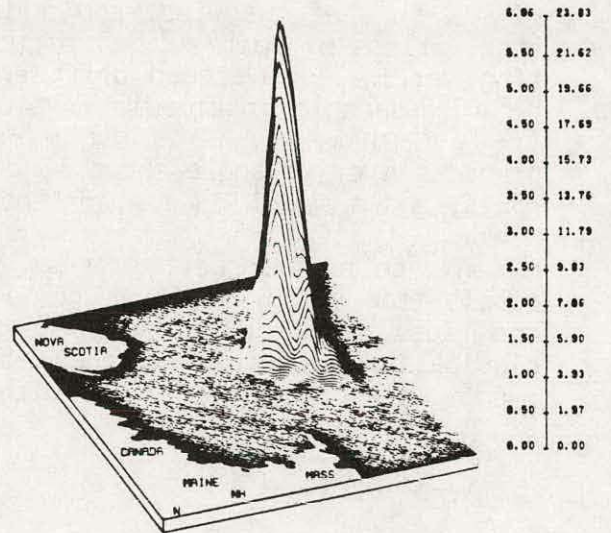


Figure 6.12 Modeled larval cod distribution for December 15.

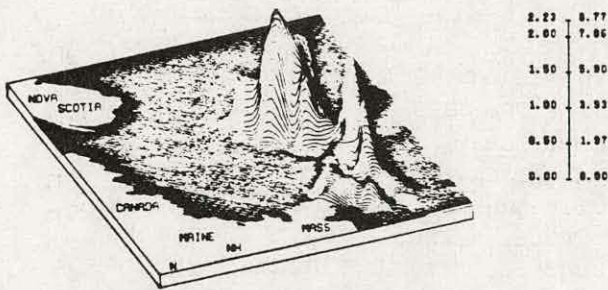


Figure 6.13 Observed larval cod distribution for February, 1975. (See caption, Fig. 11).

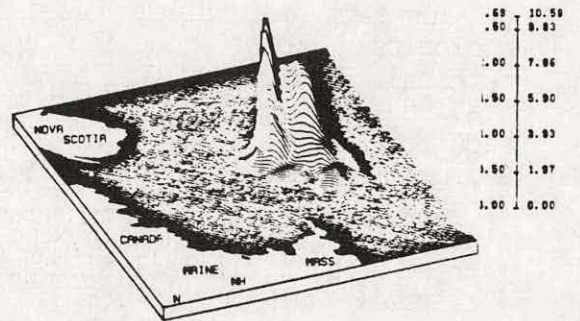


Figure 6.14 Modeled larval cod distribution for February 15.

6.2.3 THE OIL SPILL FATES MODEL

This sector of the impact model is described elsewhere in this report, and will, therefore, not be discussed in detail here. The inter-connection between the oil spill and fishery models is accomplished through storage of the oil spill output data sets on disc or tape, for access as needed by the toxic impacts section.

6.3 RESULTS OF SIMULATIONS

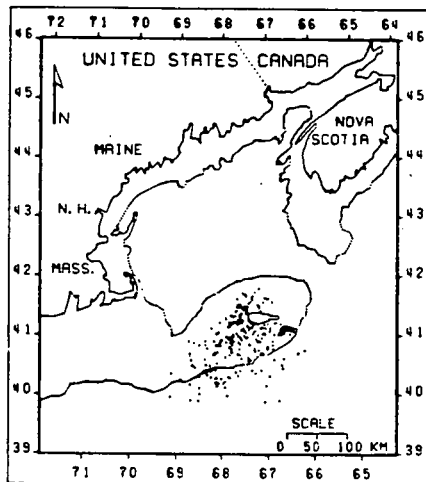
Model sensitivity to three types of parameters has been investigated. Because field data limitations and model complexity preclude the derivation of confidence intervals on the predictions, it is felt that the best indicator of reliability will be a demonstration of the relative importance of key assumptions in the system. The usual gradient approach to sensitivity (e.g. Brylinsky, 1972) is useful when the values of parameters are known with confidence intervals of, say, $\pm 15\%$. Then local rates of change due to small variations are significant. If actual parameter values may range over more than one order of magnitude, however, a set of widely spaced point values on the response surface is more revealing. This latter approach is used here.

A two-day, 34,840 metric ton oil spill, occurring on December 15, has been simulated for this sensitivity analysis. Figs. 6.15-18 show four snapshots of the interaction among the eggs and larvae, the surface slick, and the subsurface distribution of hydrocarbons within the 50 ppb contour. Further details are presented in the oil spill modeling report section. Impact predictions have been compared under three theoretically acceptable piecewise-smooth larval mortality curves (Fig. 6.4), three threshold toxicity values of 50, 100, and 1000 parts per billion (ppb) and three dispersant application scenarios in which 0%, 50%, and 100% of the oil is chemically treated. The results of these model runs are shown in Tables 6.2, 6.3, and 6.4.

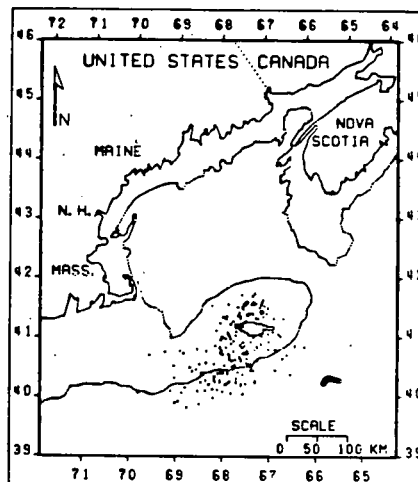
Decreasing impact is associated with increasing larval resistance to oil toxicity (increasing threshold values), with decreasing entrainment, and with increasing mortality mode. This latter fact results from an increase in the amount of compensatory mortality in modes 2 and 3 (Fig. 6.4) in the post-planktonic stages, relative to mode 1. Thus for a given treatment scenario and toxicity threshold, although the same number of eggs and larvae are lost from the system due to the spill, the effect on recruitment, and ultimately yield, is considerably different, as reflected in the relative losses associated with each mode.

Not surprisingly, none of the scenarios modeled here supports the application of dispersants as a means of mitigating impact on the fishery. Microbial degradation, which is rate dependent on both temperature and interfacial area (Traxler et al., 1977), a process not included in the oil spill fates model at this time, could alter this outcome somewhat, although to what extent is uncertain (Gibson, 1977).

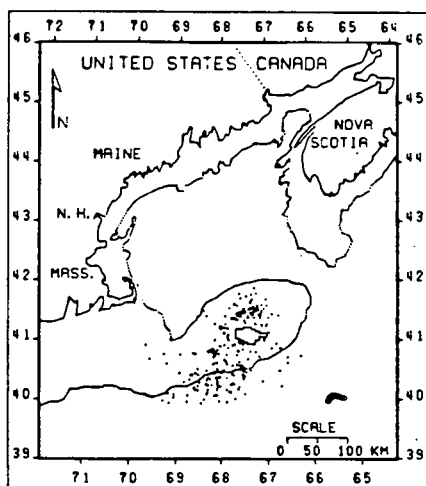
One of the more significant findings here is that the natural mortality regime for the population is more important than either threshold toxicity values or the percent of oil being dispersed into the water column. The importance of determining appropriate mortality regimes and



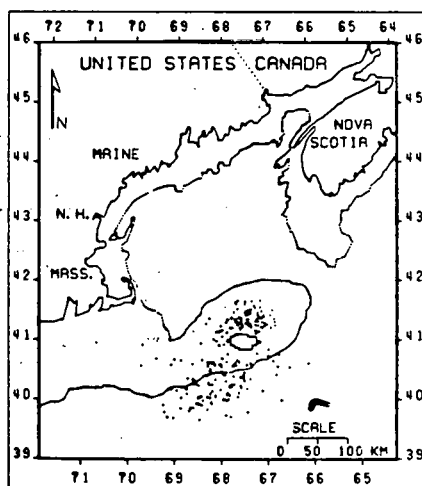
10 DAYS AFTER THE OILSPILL
(JULIAN DAY 360)



20 DAYS AFTER THE OILSPILL
(JULIAN DAY 5)



25 DAYS AFTER THE OILSPILL
(JULIAN DAY 10)



30 DAYS AFTER THE OILSPILL
(JULIAN DAY 15)

Figure 6.15-18 Four "snapshots" of the oil spill, eggs, and larvae during the simulation. The crescent-shaped group of circles is the surface slick, and the rectangular region is the sub-surface 50 ppb contour.

		Percent Chemical Treatment		
		0%	50%	100%
Threshold Toxicity	50 ppb	1.4	1.8	2.4
	100 ppb	1.1	1.4	1.5
	1000 ppb	0.3	1.0	1.2

Mortality Mode 1

		Percent Chemical Treatment		
		0%	50%	100%
Threshold Toxicity	50 ppb	0.4	0.6	0.8
	100 ppb	0.3	0.5	0.7
	1000 ppb	0.0	0.1	0.2

Mortality Mode 2

		Percent Chemical Treatment		
		0%	50%	100%
Threshold Toxicity	50 ppb	0.1	0.3	0.4
	100 ppb	0.1	0.2	0.4
	1000 ppb	0.0	0.0	0.1

Mortality Mode 3

Tables 6.2, 6.3, and 6.4: Effects of Variations Among 3 Sets of Parameters on Modeled Results. Mortality Modes refer to Curves of Figure 4. Tables entries are in thousands of metric tons lost to the Fishery. (\$1 million 1 thousand MT)

toxicity threshold values is manifest from these results. Suppose for example that an oil spill on Georges Bank were to be driven towards the islands of Nantucket and Martha's Vineyard, rather than out to sea. If mode 2 or 3 proved a good approximation to the governing mortality rates for the population, and a threshold value of 1000 ppb appeared credible for the oil at hand, treatment with dispersants before the oil reached shore would greatly decrease the aesthetic impact at little cost to the fishery. (As a "best guess" however, the most likely description of cod egg, larval, and post larval mortality on Georges Bank is a curve somewhere between modes 1 and 2, with a threshold toxicity of about 100 ppb.)

Certain limitations of the model must be stated in accompaniment to this conclusion. The most important is that only one element of the ecological complex in question is being modeled, a basic assumption being that overall biological patterns will not be disrupted by the spill. If treatment with dispersants or possible sinking of the oil resulted in contamination of the sediment on the spawning ground, this assumption would certainly be violated. The basic philosophy of causality in evolution implies that fish spawn in space and time in such a way as to optimize the probability of survival of the offspring in the long term, so that forced shifts in these patterns would presumably prove detrimental to the stock. Modeling such phenomena would require hypothesizing stock responses to extended spawning interruptions, which would fall little short of blind conjecture. Similarly, any major impact on another element of the food web could result in significant feeding shifts throughout the ecological system. An impact model of this type is, therefore, limited in its usefulness to situations involving only small population perturbations.

The magnitudes of the impacts estimated here range between 0% and 10% of the annual maximum sustainable yield of approximately 25,000 metric tons, or up to \$2.5 million in reduced income to the fishing fleet. Simulation of a 30 day oil well blowout (Reed et al., 1979b) shows impacts four times as large, so that the specific scenario is of considerable importance. Furthermore, it must be remembered that the vast majority of the commercially important species in the area, including cod, haddock, pollock, hake, herring, flounder, mackerel, lobster, crab, and scallop have pelagic eggs and/or larvae. Depending on the specific biological patterns associated with each of these species, the total cost of a spill in terms of reduction in catch could greatly exceed these values.

In summary, the simulations described here suggest that the most significant set of unknown parameters in the model system is that relating to mortality rates and processes during the first year of life. The amount of dispersant applied to the spill and the toxicity of the oil appear to be of secondary importance in deep offshore waters. (It is somewhat ironic that the most important and desirable information needed for further model improvement is also the most difficult and expensive to obtain.) As is often the case with complex simulations, the strength of the underlying data base limits the real usefulness of the output. In the case at hand, further advances in marine fisheries impact assessment of this type require a concerted ichthyoplankton data acquisition program, systematic in both space and time. Although expensive, it appears that basic progress in this field will be largely dependent on the planning and implementation of such programs.

7.0 Chemical Analysis of Oil Spills

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7.1 Introduction

The overall objective of the project is to assess the environmental impact of a chemically treated vs. an untreated oil spill. The primary objective of the chemistry group has been to determine the amounts and compositions of petroleum chemicals in the atmosphere, surface waters, water column and sediments, resulting from a treated and untreated spill. To meet this objective, it was necessary for the group to develop sample collecting, extraction, and chemical analysis methods. In addition, extensive development and testing of computer software was undertaken to collect and massage the analytical data. Laboratory experiments were designed and executed to aid in the development of these analytical techniques. Results from the laboratory studies determined the techniques which would be applied to the analysis of the meso scale experiments and eventually to any "real world" spills of opportunity.

7.2 Analytical Procedures:

7.2.1 Choice of Oil/Dispersant System

(A) Oil: The choice of oil for the study was based on several factors:

- a) availability of sufficient quantities for testing,
- b) availability of the compositional data on the oil,
- c) presence of sufficient percentages of the spectrum of representative components, e.g., aromatics, paraffinics, cycloparaffins,
- d) ability to handle oil easily at ambient temperatures.

Based on these prerequisites, it was decided that one of the two API reference crudes, South Louisiana or Kuwait, be used for the experiments. Initially, these two oils were used in laboratory tests and eventually Kuwait Crude was used for the bulk of the laboratory work and for the meso-scale experiments. In addition, as a result of two "real world" spills, bunker C oil from the Argo Merchant and a No. 2 fuel from the Buzzards Bay Spill were used in some of these studies.

(B) Dispersant:

The program objectives of the chemistry study did not include a performance testing of chemical dispersants. It was decided that a study using one well chosen dispersant and extensively testing its use with a limited number of oils would prove to be more informative and complete, vis-a-vis, the project objective, than would using multiple dispersants with these oils.

The choice of dispersants was based on several factors:

- a) product should be one of the major products on the market,
- b) dispersant should have low toxicity,
- c) dispersant should have application on wide spectrum of oil types,
- d) dispersant should be easily applied and require minimal mixing energy.

Based on the above criteria, six products were considered (Table 7.2.1). Of these, Corexit 9527, a self-mixing dispersant, was chosen for the study.

7.2.2 Infrared Analytical Procedures

- (A) Water Column
- a) Quantitative

i) Choice of solvent system - infrared analysis of the petroleum hydrocarbons extracted from the water column were analyzed quantitatively as well as qualitatively. It was desirable therefore, to have one solvent which could be used as an extracting solvent and allow for the subsequent infrared analyses without having to remove the sample from the solvent. Carbon disulfide was chosen since it can be used as an extracting solvent and has infrared spectral "windows" at 2930 cm^{-1} to allow for quantitation of the hydrocarbon band and also has windows between 1355 and 655 cm^{-1} to allow for measurement of the spectrum in the infrared "fingerprint" region (used for qualitative analysis) (1). Since the infrared cells, extraction and separation techniques required for analysis of chemically treated oil spills with this solvent were nonexistent, this lab designed and tested methods to allow us to perform infrared analyses of these samples.

The solvent was reagent grade and redistilled in glass immediately prior to use.

ii) Infrared instrumentation - analysis was performed on a Beckman 4260 Infrared Spectrometer interfaced to a Data General NOVA 3/12 Mini-computer.

iii) Design of Cell: A large portion of time was devoted to the design of 6 mm liquid cells. Cells are not normally manufactured at this pathlength and volume and cannot hold the very volatile samples and solvent we normally use. Figure 7.2.1 shows the schematic of the cell we chose. The holders were designed to contain a 6 mm spacer sandwiched between two AgCl windows. The design and material of the spacer was varied and tested as follows:

1) Teflon spacers - two Teflon spacers were machined to matching thickness (6 mm). Injection ports were located on the side of the spacer, and angled as shown as "a" in Figure 7.2.1. Teflon plugs were used to seal the ports. Two major difficulties were encountered with this design:

a) The softness of the Teflon made it impossible to machine two spacers to an exact, uniform thickness. As a result, it was necessary to hand lap the two spacers to exact thickness. This was time consuming and tedious.

b) The CS_2 slowly leaked through the side ports of the spacers.

2) Stainless Steel - two stainless steel spacers were machined to matching thickness (6 mm). Injection ports were located on the side of the spacers. Teflon plugs were used to seal the ports. The hardness of

TABLE 7.2.1 Dispersants Considered for Study

<u>Product</u>	<u>Type Oil Dispersed</u>	<u>Toxicity</u>	<u>Mixing Requirements</u>
TEOC777	Light Crudes at Sea	N/A*	Fine Mist
SURFLO-OW-1	Crude at Sea	Non-toxic	Spray/Agitate by Boat
BP1100WD	Oil at Sea only	Conforms to UK standards	Spray/seawater mix/boat
BP1100X	Oil at Sea or on beach	"	"
Corexit 7664	no limitations	"low"	Spray/Agitate by boat
Corexit 9527	no limitations	"low"	None required

*N/A-none available

All information was taken from company product brochures.

AgCl CELLS WITH STAINLESS STEEL SPACERS

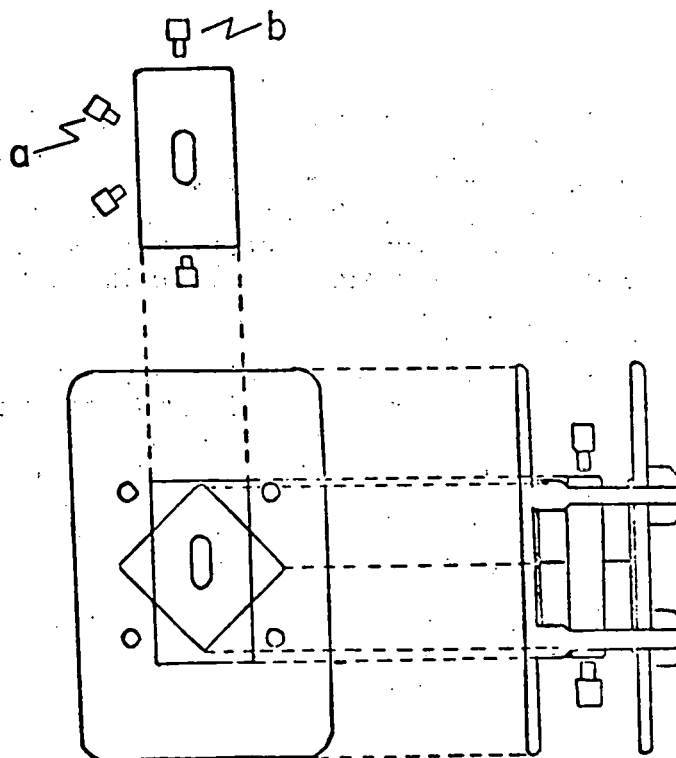


Figure 7.2.1 AgCl Cells with Stainless Steel Spacers

the stainless steel allowed for machining of the two spacers to exact thickness and, unlike the Teflon, no further polishing was necessary. However, the ports still leaked.

(3) Stainless Steel - two stainless steel spacers were machined to matching thickness. The port positions were moved from the sides to the top and bottom, as "b" in Figure 7.2.1. This prevented leakage. The cells presently in use are those designed with ports located on the top and bottom of the spacer.

iv) Extraction Efficiencies

To determine the extraction procedure and the amount of solvent that would yield a relatively high extraction efficiency, four procedures were tested, using carbon disulfide as the extracting solvent. In each experiment, one liter of sea water collected from a previously determined clean site was spiked with a known amount of sample and poured into a 2000 ml separatory funnel. The organics were then extracted as follows:

a) Ten mls. of CS_2 were added to the water and the sample was agitated for 5 minutes. The bottom organic layer was transferred to a 25 ml volumetric and brought to volume with additional solvent.

b) Ten mls. of CS_2 were added to the sample in 5 ml portions with extraction after each addition. The 5 ml portions were combined in a 25 ml volumetric and brought to volume with additional solvent.

c) Fifteen mls of extracting solvent were added to the sample in 10 and 5 ml aliquots, with extraction after each addition. The aliquots were combined as described above.

d) Thirty mls. of extracting solvent were added in 15 ml aliquots, with extraction after each addition. Combination of sample and volume adjustments were made as described above.

The amount of extracted hydrocarbon in each sample was determined by measurement of the absorbance of the 2930 cm^{-1} band.

These four procedures were tested with Kuwait Crude, Corexit 9527 dispersant and a 5:1 mixture of Kuwait Crude and Corexit 9527. Results are shown in Table 7.2.2. As can be seen, method "d" yields the highest efficiency. All extractions are now performed according to this method.

v) Analytical Protocol

In the initial phases of the project, the feasibility of chemically separating the oil from the dispersant prior to infrared analysis was studied. The dispersant is a mixture of polar hydrocarbons, whereas the oil is a mixture of nonpolar and polar hydrocarbons (the nonpolar compounds being present in the higher percentage). Therefore, Thin Layer and Column Chromatography were used with various solvent systems in an attempt to isolate the oil from a mixture of oil and dispersant. Several pure solvents and solvent systems were tested for their resolution capabilities. The best results were obtained with a system of a 1:1 mixture of $CHCl_3:CCl_4$. However, even with this system, a complete separation

Table 7.2.2. Results from Extraction Efficiency Experiments

<u>Procedure</u>	<u>Efficiency</u>		
	Kuwait Crude	Corexit 9527	Kuw/Corex
a) 10 ml 1st ext. 0 ml 2nd ext. <u>10 ml total</u>	40.5%	8.7%	28.8%
b) 5 ml 1st ext. 5 ml 2nd ext. <u>10 ml total</u>	31.0%	10.3%	21.8%
c) 10 ml 1st ext. 5 ml 2nd ext. <u>15 ml total</u>	31.8%	11.1%	46.6%
d) 15 ml 1st ext. 15 ml 2nd ext. <u>30 ml total</u>	64.8%	22.0%	65.2%

of the oil from the dispersant could not be realized. Because of this and of the time required to perform this separation, it was decided that development of computer techniques to effect spectral separation of these two components would be more promising (see Section 12.5).

The amount of hydrocarbons present in a sample was determined by placing 0.5 ml of the sample solution into the sample cell. The matched reference cell was filled with CS₂ and both were placed in the infrared spectrometer. Since the cells were of identical pathlength, the CS₂ absorbed the same amount of light from both sample and reference beams, effectively eliminating the bands due to the solvent and allowing the measurement of the absorbance band for hydrocarbons at 2930 cm⁻¹. The absorbance of the 2930 cm⁻¹ band was calibrated using solutions of known concentrations of the oil, oil/dispersant and dispersant respectively, and concentration vs. absorbance curves were plotted. The concentration of the unknown was then determined from the appropriate curve.

b) Qualitative - Spectral measurement

Following quantitative analysis, the total sample is concentrated to approximately 1 ml by slowly evaporating the solvent. Again, about 0.5 ml of this solution is placed in the sample cell, pure CS₂ is placed in the reference cell. Both are placed in the instrument and the infrared "fingerprint" of the sample is measured by scanning the 1355-655 cm⁻¹ region of the spectrum.

(B) Air

a) Charcoal Tubes

i) Laboratory

The vapors above treated and untreated simulated oil spills were collected by pumping air above the slick through activated charcoal cartridges. A flow meter was connected between the cartridges and a pump to measure flow rate. Three systems were used for collecting vapors:

- 1) the apparatus shown in Figure 7.2.2.
- 2) the apparatus shown in Figure 7.2.2 without the charcoal filter.
- 3) the apparatus shown in Figure 7.2.3.

Prior to the extraction of the charcoal an internal standard, n-C₂₀ (eicosane), was added to the solvent. Carbon disulfide was used for extraction. Thus, its area and height can be easily determined. The concentration of the standard was about 50 ppm. Before the extraction, the solvent and the charcoal were cooled in liquid nitrogen and then mixed together. This was done to prevent losses of vapors due to heat of extraction (1). Extraction time was 30 minutes. Infrared spectra were measured using the 6mm cells described above. Carbon disulfide was used as a solvent for the IR measurements.

ii) Meso scale

Two tanks, 6.2 meters tall and 0.9 meters in diameter, located about 50 meters from the Narragansett Bay, were used for the meso-scale experiments. The tanks were filled with approximately 2000 liters of sea water pumped from the ocean. Kuwait crude oil was added to the north and south tanks, and Corexit 9527 was then added to the south tank.

The surface was mixed by stirring with glass rods. Air samples were collected immediately after the spill. Air samples were collected and treated similarly to the air samples taken in the laboratory experiments. Figure 7.2.4 shows the system used for collecting the air samples in meso-scale experiments. The funnels through which the air was pumped were placed at about 2.5 cm above the water surface.

Extraction of samples from the charcoal tubes and infrared analysis of the samples were performed as described above.

b) Long-path Gas Cell

The purpose of this study was to determine the feasibility of direct IR monitoring of vapors of oil and its various light hydrocarbon components. Fundamental problems are quickly encountered when trying to obtain an IR spectrum of a complex mixture such as crude oil. Overlapping bands and non-linear responses make quantitative accuracy questionable in such cases, and this was one of the major problems addressed. Work was largely done with synthetic mixtures of light hydrocarbon gases to simplify the study. Problems of sample handling and transfer were also addressed. A simple laboratory system was set up for the routine analysis of vapors from liquid hydrocarbon samples, along with special handling apparatus for other situations (artificial weathering, etc.). Finally, a simple, very small-scale spill simulation tank was set up.

Spectra were measured on a Beckman 4260 infrared spectrophotometer with a Wilks 20-m Variable Path Gas Cell mounted in the sample beam. A beam attenuator was placed in the reference beam and the sample compartment was continuously flushed with dry N₂ gas to minimize atmospheric interferences.

Figure 7.2.5 shows a simple schematic of the 20 m gas cell. The IR sample beam is directed up into the cell, multiply-reflected along the length of the cell, and directed back out and into the instrument. By

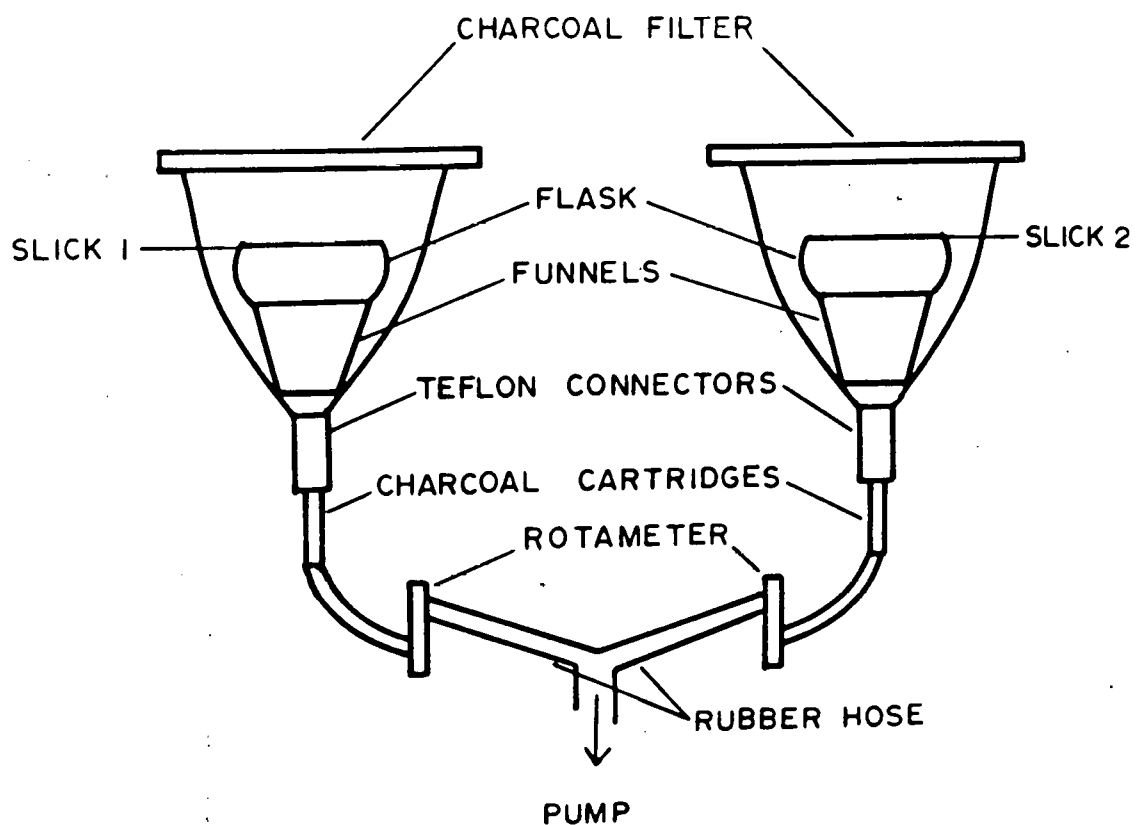


Figure 7.2.2 Air Flow Sampling Probe for Laboratory

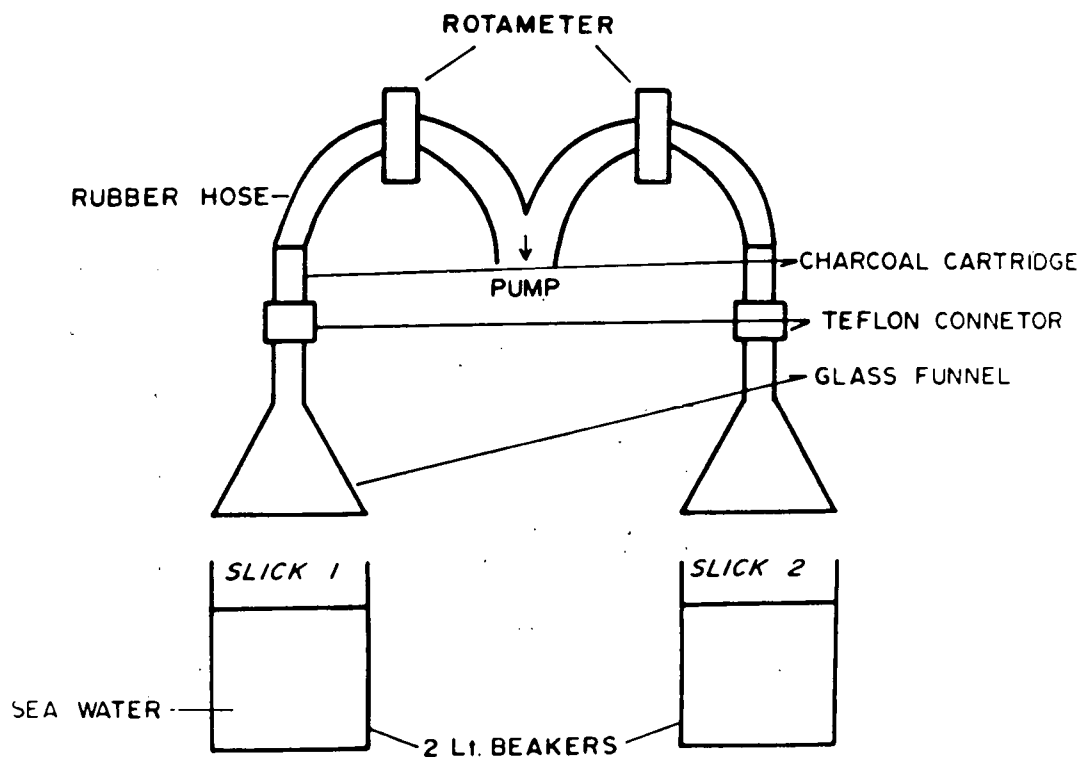


Figure 7.2.3 Test with Prefiltering for Laboratory Experiment

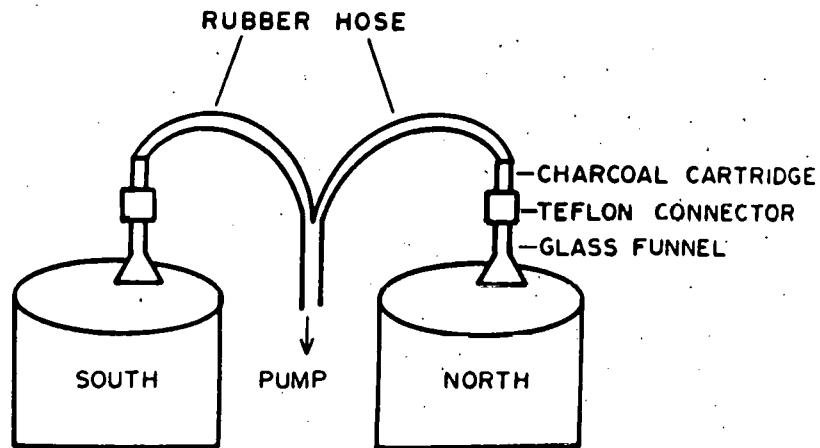


Figure 7.2.4 Test with Prefiltering for Meso Scale Tank

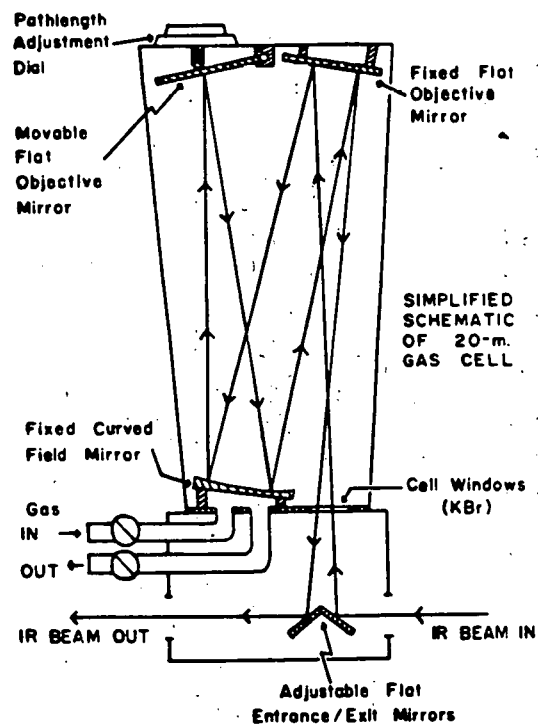


Figure 7.2.5 Schematic of the IR 20 meter Gas Cell

varying the angle of one mirror with a simple vernier dial, the number of reflections and, therefore, the pathlength in the cell, can be varied. The pathlength can be set from 0.75 to 21.75 m, in increments of 1.5 m. The longer pathlengths are often necessary when working with low concentrations or weakly absorbing species. Two gas connections, with valves, allow for a flow-thru operation of the cell. The cell is about 0.4 m long, with a volume of 5.5 liters.

Figure 7.2.6 shows a diagram of the experimental setup. The apparatus can be used in several ways. For quantitative studies of pure gases, dry N_2 was pumped through the cell to flush the system. The 4-way valve was then turned to isolate the pump and gas cell (in a closed loop) and a sample of gas was injected through the septum with a gas syringe. Repeated injections of a gas into this flowing loop could be made while monitoring a wavelength of interest on the IR, until the desired concentration was reached. Likewise, sequential injections of different gases could be made to produce a synthetic mixture of known composition. Injections were made with Series A gas syringes from Precision Sampling, Inc. Syringes were filled from lecture bottles via a stainless steel outflow tube.

For sampling vapors from crude oil or from a simulated oil spill, the vapor is pumped once through the cell and out the exhaust. In the case of a spill a glass funnel suspended over the spill is connected to the input. For pure oil samples, a sampler such as in Figure 7.2.7 can be used to isolate the vapors. All pump parts, valves and connections are 316 stainless steel and tubing connections are made with TFE. The gas cell itself is Teflon lined.

Data measurement was generally carried out with the IR interfaced to the Data General NOVA 3/12 computer. Programs developed in the lab allow for acquisition and storage of data, spectral smoothing, addition or subtraction and graphic display of spectra on a CRT or plotter. This allows for improvement and enhancement of spectral display, and exact comparisons of very similar spectra. Also, spectra of pure gases can be added in the computer to produce an artificial mixture, for comparison with a real sample.

Most work with pure light hydrocarbons was done from 3250-2750 cm^{-1} in the region of the C-H stretching frequency. Some work with heavier hydrocarbons was done in the fingerprint region from 1000-500 cm^{-1} . Light hydrocarbons used were methane, ethane and propane, while benzene and toluene were used as heavier aromatic hydrocarbons. Data for the computer was acquired at 1/10 cm^{-1} increments over 500 cm^{-1} , giving 5000 data points. Spectra of larger regions were also measured at 1 cm^{-1} resolution. Typical IR conditions were: 50 cm^1/min , 1.5 cm^{-1} resolution; pathlength from 0.75 to 21.75 meters.

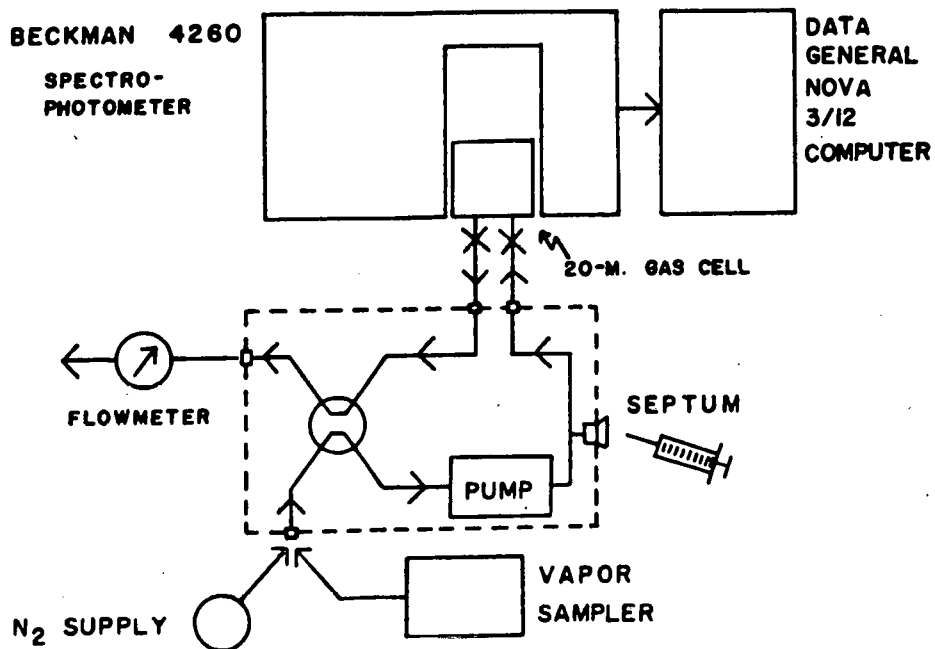
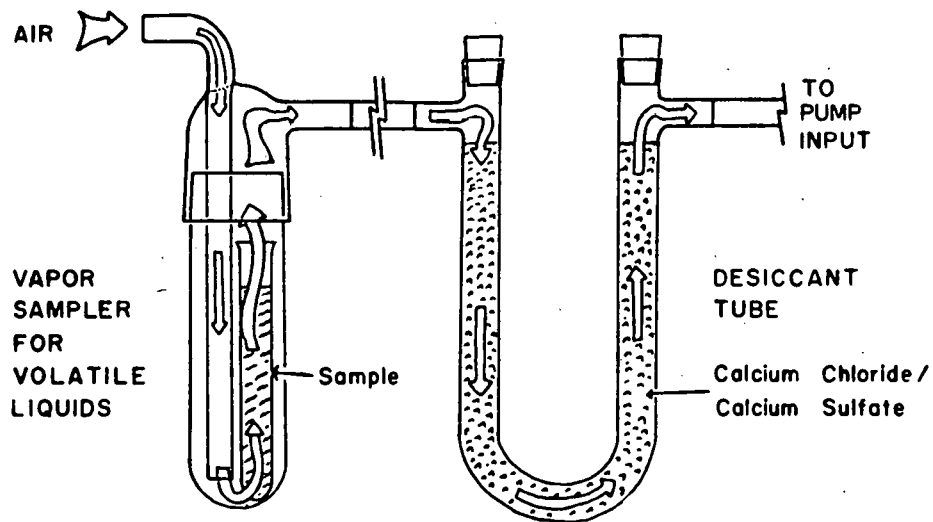


Figure 7.2.6 Diagram of IR System



VAPOR SAMPLER AND DESICCATOR

Figure 7.2.7 Vapor Sampler and Desiccator

7.2.3 G.C. Analytical Techniques

Qualitative/Quantitative Procedure

(A) Water Column

After infrared analysis was completed, the CS_2 was completely removed from each of the extracts by evaporation and the residue was taken up in 2 μ liters of hexane.

The samples were then analyzed by Gas Chromatography (GC) on either a Hewlett Packard Model 5710A or a Perkin Elmer Sigma 2, both equipped with flame ionization detection and 10-m by 3-mm column packed with SP2250 (temperature programmed at 8 degrees C/MIN).

(B) Air Analysis

a) Separation on GC followed by IR - prior to extraction of the sample impregnated charcoal. an internal standard, $n-C_{20}$ (eicosane) was added to the solvent, CS_2 . Eicosane was chosen since its GC peak does not overlap any of the GC peaks of the sample, thus its area and height can be easily determined. The concentration of the standard was about 50 ppm. Gas chromatograms were measured using a Hewlett-Packard Model 700. The GC was modified for collecting fractions. The GC is equipped with a 10 ft., 1/8 in. column of 10% SP2250 on 100/120 Supelcoport and a flame ionization detector (FID). The detector destroys the eluents, therefore, it was necessary to split the effluent prior to the detector. A Swagelok union T was inserted between the column and the detector (inside the oven) to split the flow valve. A stop-flow valve was placed between the splitter and the FID detector. Another stop-flow valve and a fine metering valve (Nupro 4BM) was installed between the splitter and the device. The splitter and all three valves were located in the oven; however, the metering valve could be controlled externally. A schematic of the oven compartment is shown in Figure 7.2.8.

After the two valves on the collection side of the splitter, the effluent exits the oven compartment through a temperature controlled heated jacket to the "merry-go-round" device shown in Figure 7.2.9. This device was made in-house of Teflon; the eluent enters the device through the center and is directed at a right angle to the front where it enters one of the 20 possible holes containing a charcoal cartridge.

To collect a number of fractions, the GC eluents were monitored by the FID detector (10% going to detector, 90% to the collection device). When the recorder indicates that a GC fraction was starting to elude the column, the collection device is manually moved to a position containing the desired charcoal cartridge. The eluent was collected and the device was rotated to another position for collecting the next fraction.

The possibility of a single component concentration exceeding the breakthrough level of a charcoal cartridge was investigated for a number of components by attaching a second cartridge to the exit of the first cartridge. The components could not be detected in the solutions of the desorbed cartridges; thus, it was concluded that under typical GC conditions the breakthrough level would not be exceeded.

Figure 7.2.8 GC Column Arrangement in Oven

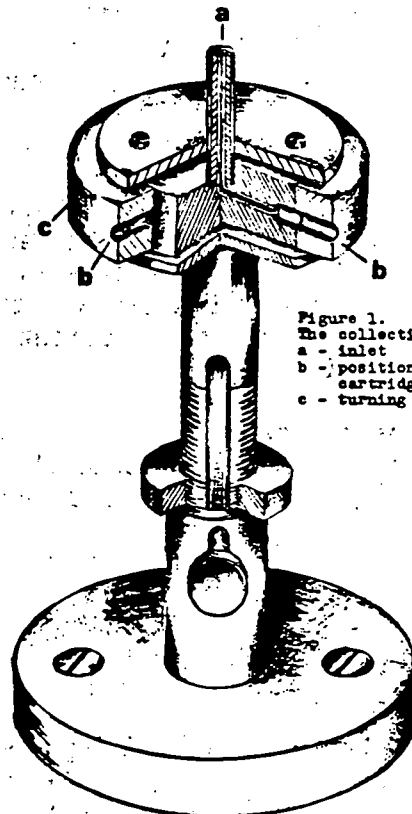
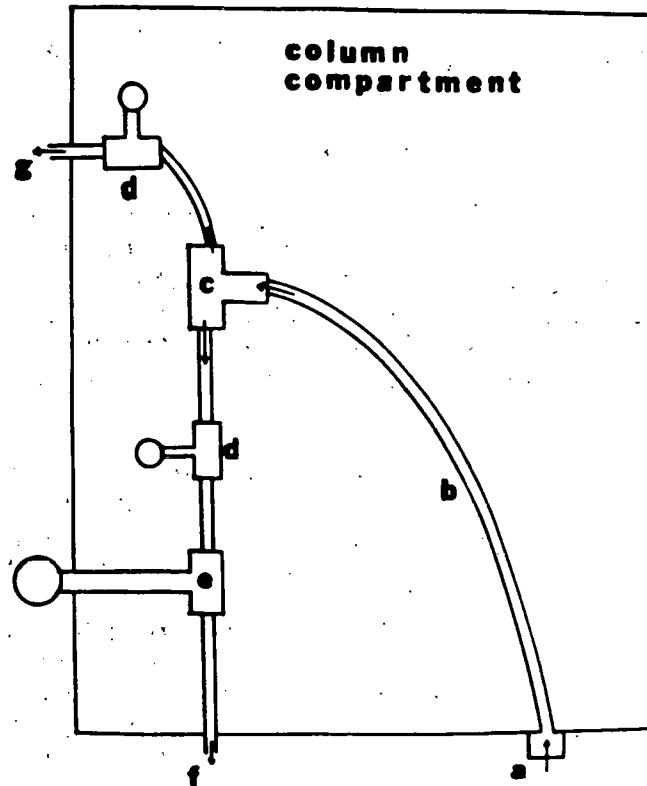


Figure 1.
The collecting device.
a - inlet
b - positions of charcoal
cartridges
c - turning part

Figure 7.2.9 Device for Collecting Gas Samples

h) IR analysis, followed by GC of total sample - subsequent to infrared analysis of the charcoal extract. gas chromatograms were measured on either the Hewlett Packard 700 or the Hewlett Packard 5710A, both previously described.

7.2.4 GC-Mass Spec Analytical Procedures

The GC/MS/CS system was developed in order to analyze water extract samples for aromatic hydrocarbon compounds. The MS is of the chemical ionization (CI) variety and is ideally suited for aromatic compounds. The nucleophilic nature of these compounds increases the reaction cross section and enhances the sensitivity. Also the nature of the CI process yields a strong molecular ion peak and, therefore, is readily interpretable.

CI is a phenomenon resulting from ion-molecule interactions and requires gas mixture pressures on the order of one Torr in the MS ion source. The composition of the gas is such that the reagent gas, in this case CH_4 , is present at a much higher concentration than the sample. Primary ionization occurs in the reagent gas because of its great excess through electron impact ionization. These reagent ions then react with reagent gas in second order processes to produce stable ions characteristic of each gas (for CH_5^+ and C_2H_5^+). These reagent ions are stabilized as a plasma in the ion source and there are no further reactions of these characteristic reagent ions with the reagent gas.

When a reagent ion encounters a sample molecule, one of several chemical interactions may occur. These include transfer of a proton, a hydride ion, another ion fragment, or a charge. One important advantage in CI as opposed to electronic impact (EI) is that the average energy transferred to the sample molecule by the reagent ion is much less than that transferred by EI ionization and this leads to only a small amount of fragmentation and, therefore, a large molecular ion peak.

A chemical ionization system can be readily interfaced with a gas chromatograph. Because the source operates at high pressures, sample separations can be eliminated and the entire effluent from the GC can be introduced into the ion source. Because of the vast amounts of data produced by a GC/MS system, a dedicated computer system for control and data acquisition is a necessity.

The objectives were as follows:

- a. Assemble the MS system with its associated vacuum system, cooling systems, electrical and electronic system and sample handling systems.
- b. Interface a gas chromatograph to the sample inlet of the MS and determine the optimum columns and conditions for operations.
- c. Interface the GC/MS to a computer system and develop the necessary hardware and software to support such a system.

A HP-5710A gas chromatograph with capillary column pneumatics was used to separate the extract mixtures prior to MS analysis. A J Scientific SP--2250 glass capillary column was finally chosen as the most versatile and efficient column for the separation of a low to medium

mass aromatic hydrogen. Temperature programming was from 90° to 270°C at 4 C/min. The carrier gas was helium. The injector was automatically purged 45 seconds after injection.

The MS was a Biospect/Finnegan with a CI source and a quadrapole mass separator. A complete MS scan from 50 to 400 amu was performed three times per second and this data was stored by computer. The scan rate was controlled by the computer through a DAC. The rate could also be manually controlled by the operator. The GC effluent was introduced directly into the MS source through a heated glass lined tube. The solvent peak was not vented to the atmosphere, rather the source filament was turned off while the solvent was passing into the MS. This was easily monitored via the source pressure gauge.

The computer system was a Data General Corp. NOVA3/12 with 64K word memory, foreground/background and memory map protection, 10M byte cartridge disk system, 16 channel 12 bit ADC, 2 channel 12 bit DAC, 16 channel digital I/O, CRT, TTY, and a plotter. The software used was DGC Fortran IV and DGC Nova assembly language. The Fortran was used mainly for data management, processing, and display. The assembly language was used for data acquisition and instrument control.

Figure 7.2.10 is a typical mass spectrum scan of a several component mixture containing PAH. The identified compounds are toluene, phenanthrene, anthracene, fluoranthrene, pyrene, triphenylene, benzanthracene and chrysene. This spectrum was obtained using the solids probe and was used as a calibration scan.

Figure 7.2.11 is a total ion plot showing the reconstructed gas chromatogram for an n-paraffin calibration mixture.

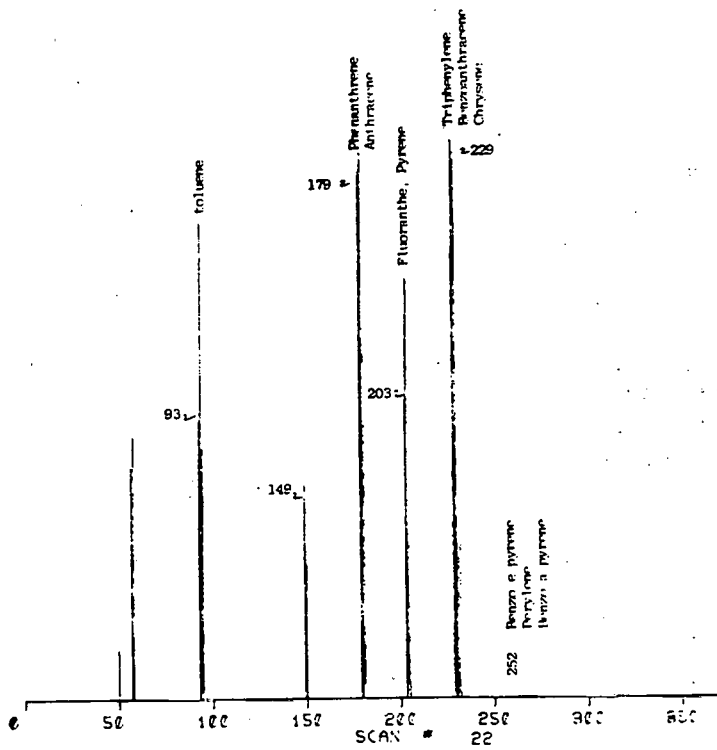
Figures 7.2.12 and 13 show the total ion plot and subsequent mass spectrum for a sample of dimethyl-naphthalene in hexane. As can be seen from the total ion plot, a compound is indicated by a GC peak at 390th scan. The mass spectrum of scan 390 indicates a molecular ion mass of 157 amu which corresponds to the dimethyl-naphthalene.

Figure 7.2.14 shows the total ion plot-reconstructed gas chromatogram for the aromatic fraction of a fuel oil. Naphthalene, methyl naphthalenes, dimethyl-naphthalenes, tri-methyl naphthalene and phenanthrene can be clearly and unambiguously identified.

Figure 7.2.15 shows the total ion plot of deasphalted Kuwait Crude oil in hexane. Benzene, xylene, naphthalene, methyl-naphthalene and dimethyl-naphthalene can be identified along with the n-paraffins.

Figure 7.2.16 shows the total ion plot for a water extract from the south tank top after one hour. Xylene, naphthalene, methyl-naphthalene, and dimethyl-naphthalene along with n-paraffins were detected.

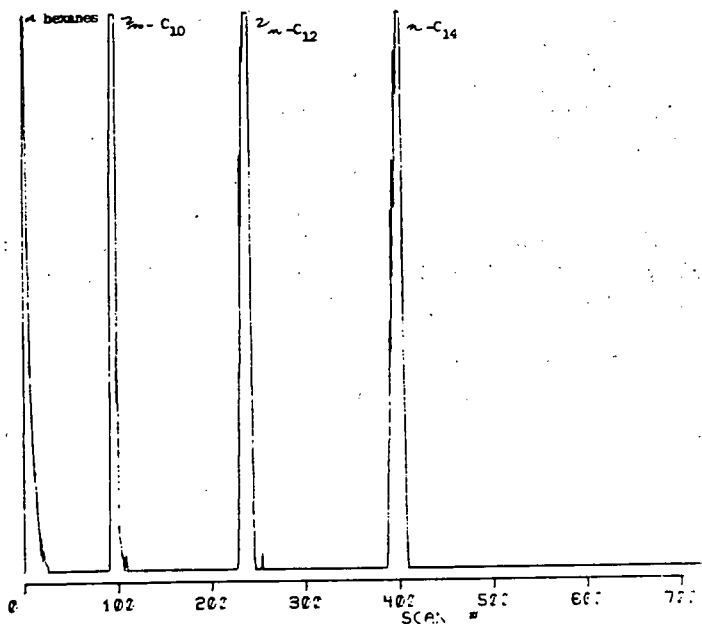
Figure 7.2.17 shows the total ion plot for a water extract from the South tank top after 24 hours. Naphthalene, methyl-naphthalene, dimethyl naphthalene along with n-paraffins were detected.



PAHSTD
Solids Probe
28 Nov. '78

calibration off by + 1

Figure 7.2.10 Typical Mass Spectrum of a Several Component Mixture Containing P, A. H.

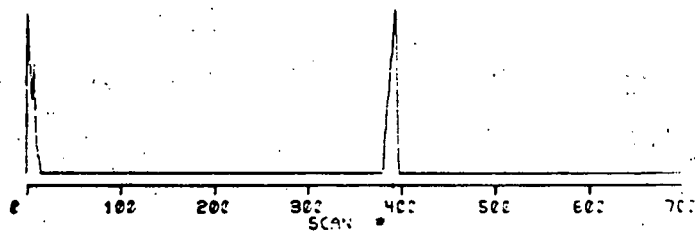


1 ml C₁₀C₁₂C₁₄ in hexane
11 Oct. '78

Total : 1 V
50 lower limit

90 to 270°C @ 8° C/min
20 psi SP-210⁰ glass capillary
C H₄ @ ~ 1000 milliliter @ source

Figure 7.2.11 Total ion plot showing the reconstructed Gas Chromatogram for an n Paraffin Calibration Mixture



Dimethnap (Dimethyl-naphthalene)

13 Oct. '76

Totlon : 1 X

50 filters
700 scans

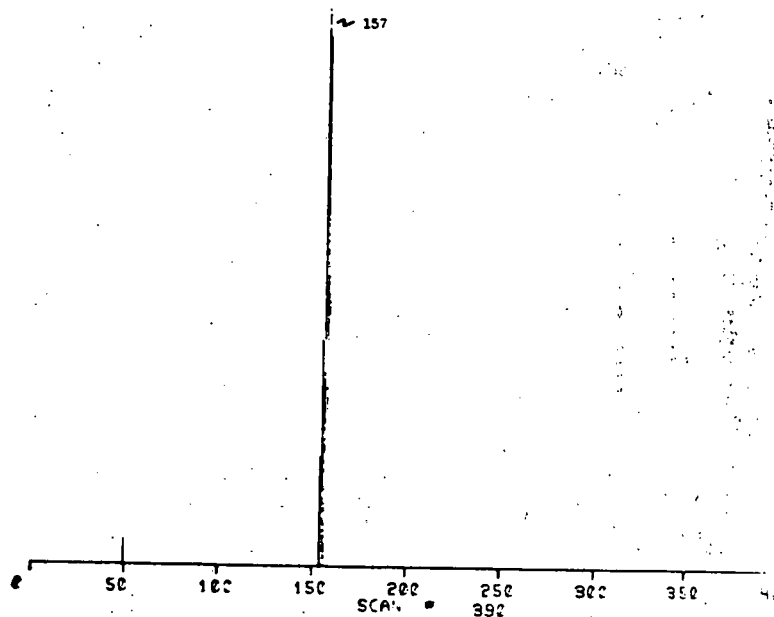
CH₄ @ ~ 1000 milliliter @ source

90 to 270°C @ 8°C/min.

capillary column SP-2100

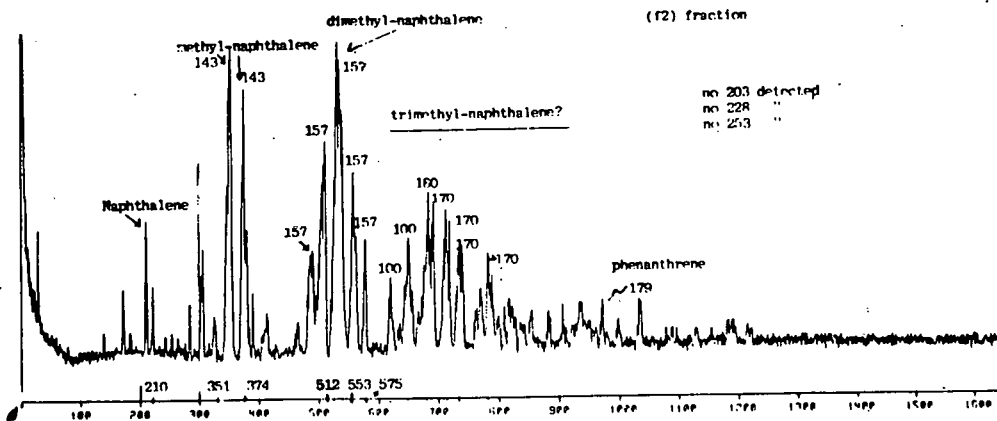
35 psi

Figure 7.2.12 Total Ion Plot for the Sample of Dimethyl-naphthalene in Hexane



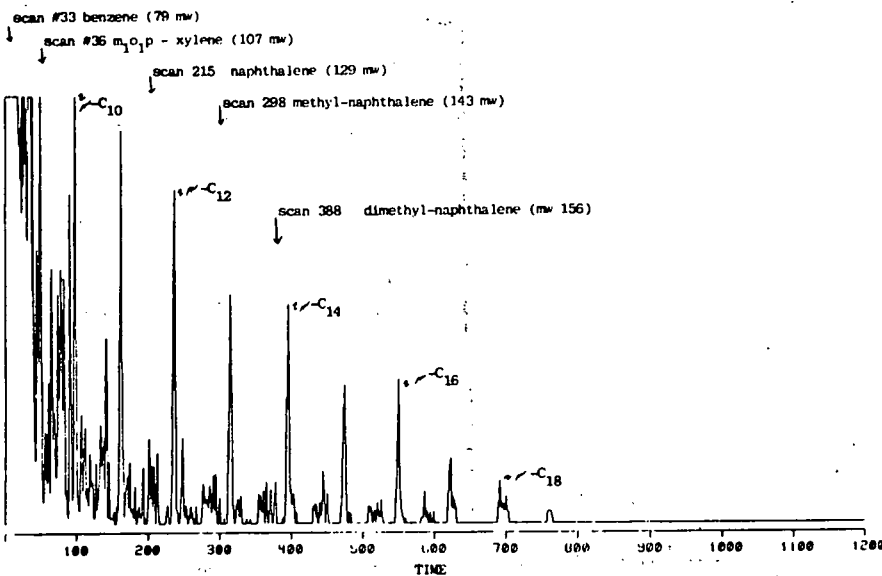
Dimethyl-naphthalene

Figure 7.2.13 Mass Spectrum of Scan 390



6 Feb. '79
50 limit on tot ion
1" limit on ms displays

Figure 7.2.14 Total ion Plot Reconstructed - GC for Aromatic Fraction of Fuel Oil



Kuwait (Deasphalted in Hexane) 16 Oct. '78
Tot ion : 1 X
50 filters

90 to 270°C @ 8°C/min.
25 psi SP-2100 glass capillary
CH₄ @ ~1000 milliliter @ source

Figure 7.2.15 Total ion Plot of Deasphalted Kuwait Crude Oil and Hexane

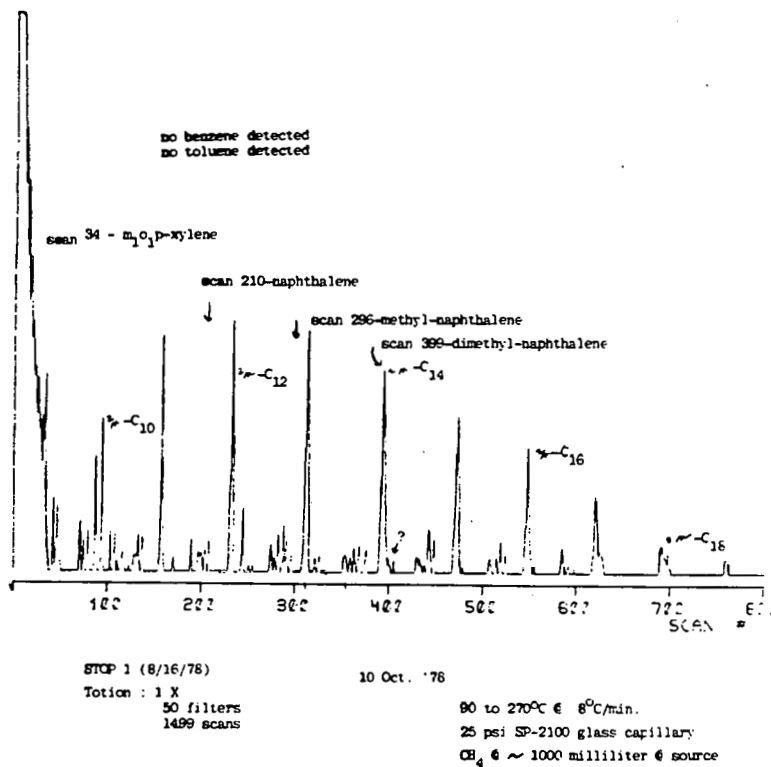


Figure 7.2.16 Total ion Plot for a Water Extract from the South Tank after one hour

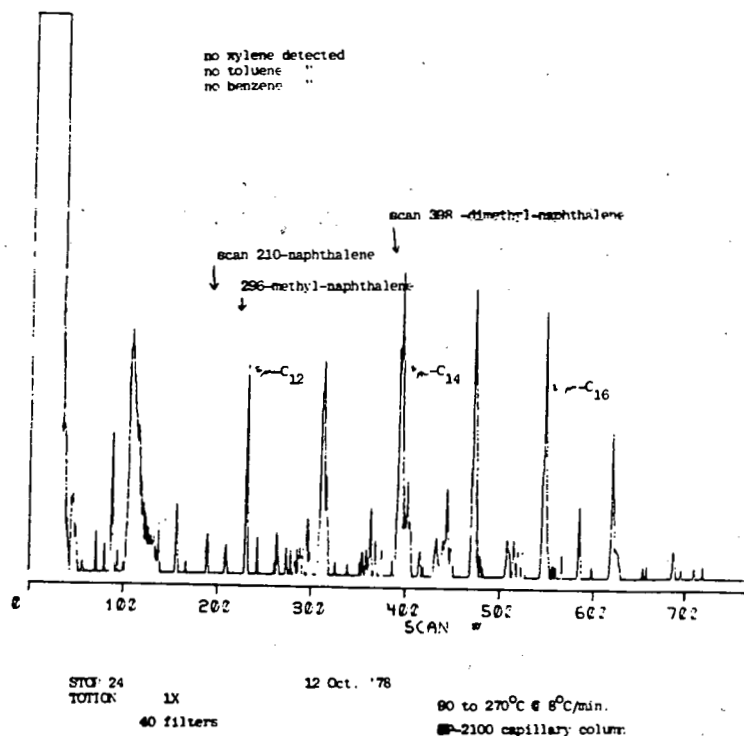
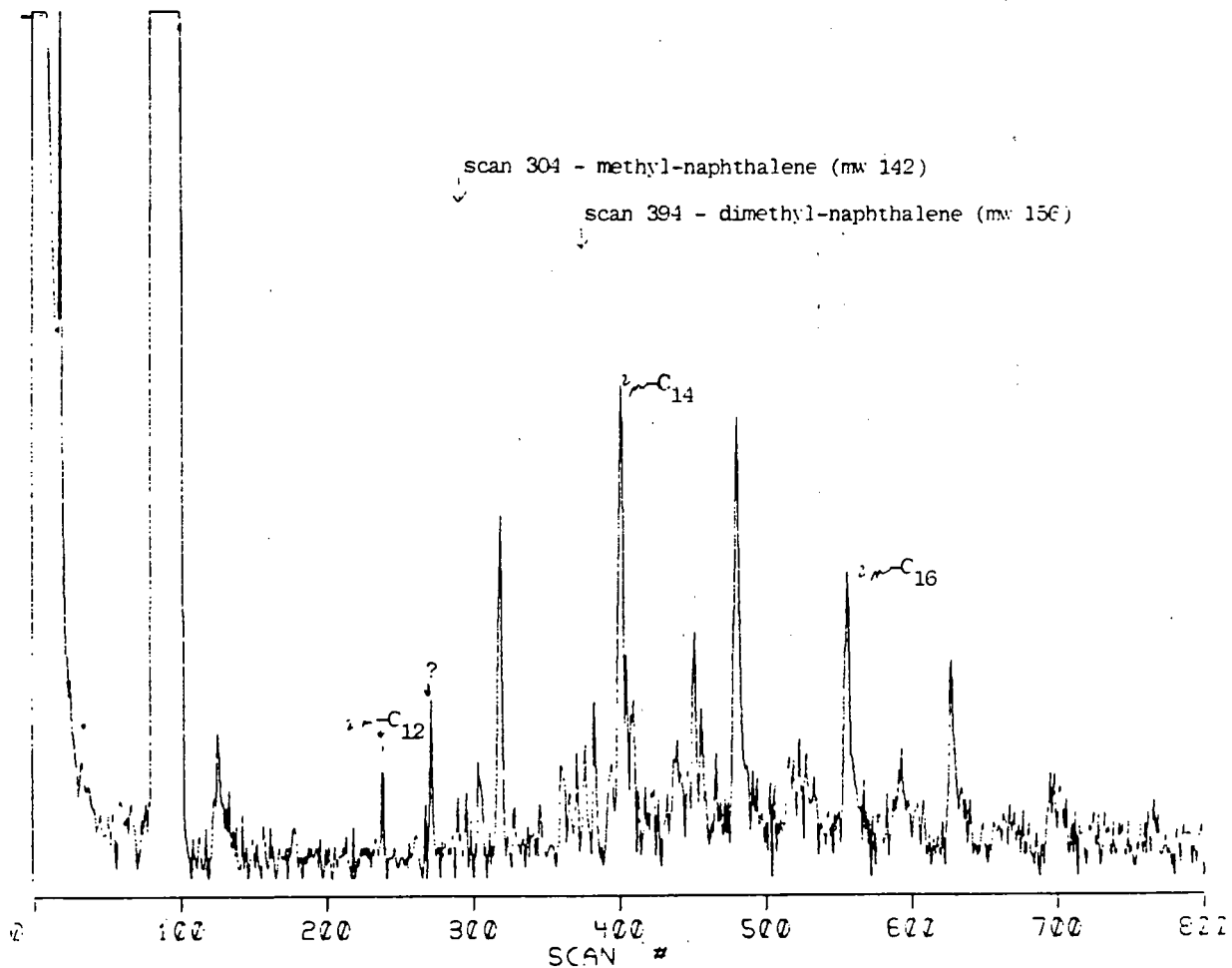


Figure 7.2.17 Total ion Plot for a Water Extract from the South Tank after 24 hours

Figure 7.2.18 shows the total ion plot for a water extract from the south tank mid after 24 hours. Methyl-naphthalene, dimethyl-naphthalene, along with n-paraffins were detected.

no benzene detected
no xylene detected
no naphthalene detected



SMID 24

18 Oct. '78

TOTION 3 X
15 filters

90 to 270°C @ 8°C/min.
SP-2100 capillary column

Figure 7.2.18 Total ion plot for Water Extract from the middle of South Tank after 24 hours

7.3 Laboratory Experiments:

The laboratory experiments were intended to:

- 1) test the available methodology
- 2) develop new methods
- 3) be used as cursory analyses of the oil/dispersant system to provide an overview of the analytical problems that would be encountered and the results that may be anticipated in the meso-scale and "real world" environments.

For these experiments, untreated and chemically treated spills were manufactured in laboratory scale test tanks and in larger, outdoor tanks. The oils used in the experiment were API Kuwait Crude, API South Louisiana Crude; the No. 6 oil involved in the Argo Merchant Spill (Dec., 1976), and the No. 2 oil from the Buzzards Bay Spill (Jan., 1977).

7.3.1 Water Column

(A) Methodology:

Effect of dispersant on Kuwait Crude and S. Louisiana Crude: Four fiberglass containers were filled with 28 liters of Narragansett Bay sea water. Vertical agitation of the water was provided by the vertical motion of Al paddles hinged to the bottom of each container and attached to a motor via a nylon string. Ten ml. of each oil were placed in two test tanks and 10 ml. oil/2ml dispersant were placed in two other test tanks. Qualitative results on the second laboratory experiment are given in Table 7.3.1. The total relative amounts of petroleum entering the water is about the same for the two oils. A large amount of phthalic acid esters (phthalates) were found in the Kuwait test tank after 24 hrs., the source of which could not be traced.

(B) True solubility of petroleum chemicals:

For this series of experiments, "artificial sea water" was used and was prepared by adding a specified amount of Instant Ocean (Aquarium System, Inc., Ohio) to distilled water. Oil was added to the surface of the water contained in a large glass carboy. The water was gently agitated with a slowly moving magnetic stirrer for the duration of the experiment.

The results for two different initial concentrations of So. La. Crude are given in Figure 7.3.1. Two 1 liter water samples were collected prior to each experiment (controls or C), two subsurface samples at 1 hour, and two at 24 hours. One 1 liter sample from each time period was analyzed without filtering and the other was filtered through a 0.45 mm Millipore filter prior to analysis. The filtering was performed in order

Table 7.3.1

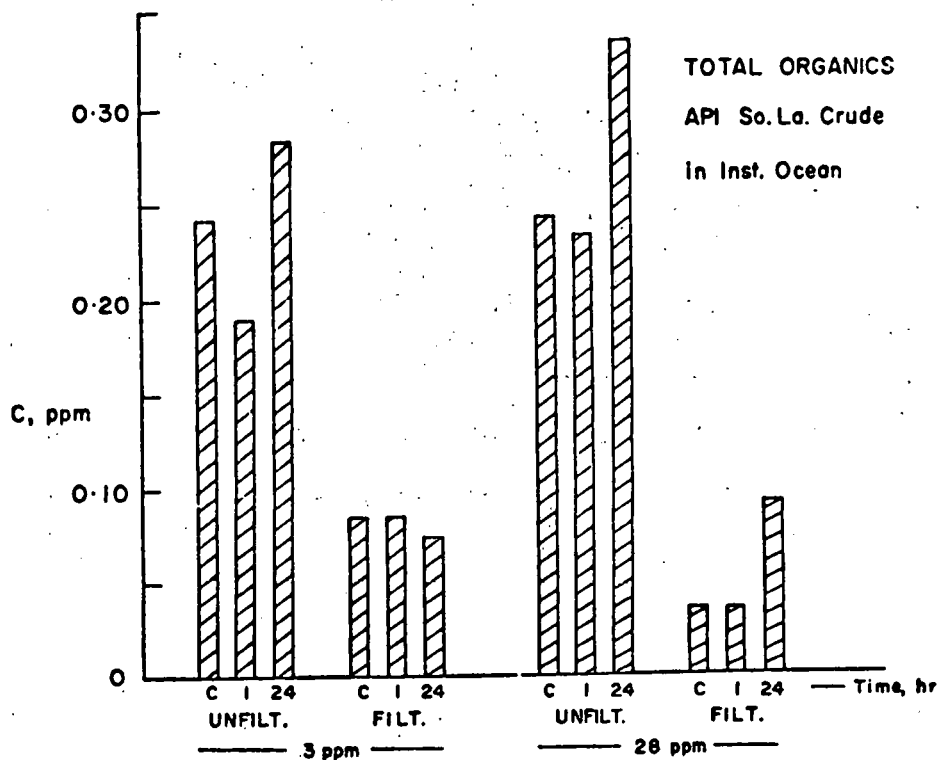
Qualitative Results of 2nd Laboratory Experiment

Test System	Relative Amounts of Oil Present ^a	
	1 hour	24 hours
Kuwait Crude	1	High in Phthalates (some oil)
Kuwait/Disp.	3	7 ^b
So. La. Crude	1	2
So. La. Crude	3	7

^aEstimated from IR spectra

^bAfter separation by column chromatography

Figure 7.3.1 Total extractable Organics from Laboratory Experiment on South Louisiana Crude Oil with Initial Concentrations of 6 and 28 ppm.



to remove dispersed droplets; however, the control also contained considerable amounts of filterable particles.

Starting with 3 ppm of the crude oil (e.g., 15 mg of oil added to the surface of 5L. of water) we observed an overall increase in total organics after 24 hours; however, after filtering, the controls, 1 and 24 hour samples contained (within experimental error) the same amounts of extractable organics. In the experiment with an initial concentration of 28 ppm, the total organics in the unfiltered water increased by 0.094 ppm and those in the filtered water by 0.056 ppm after 24 hours in the filtered water. These two experiments indicate that the relative amounts of soluble organics in oil is low; however, directly beneath a slick, soluble compounds can be found as is indicated in the 28 ppm experiment.

We performed the same experiment with the No. 6 oil from the Argo Merchant spill. In this case 6.2 ppm of the oil were added to the artificial sea water; the results are presented in Figure 7.3.2. Again, the amount of oil entering the water was small; the amount of total extractable organics in the filtered water increased by 0.020 ppm after 24 hours.

The same experiment was performed with the No. 2 fuel oil from the Buzzards Bay spill. The results are presented in Figure 7.3.3. The initial concentration of 24.7 ppm is similar to the second So. La. Crude oil experiment and the results are similar. There was an increase in the total organics in the unfiltered water after 1 and 24 hours. Furthermore, the true solubles increased by 0.035 ppm after 24 hours in the filtered water.

Another useful result can be obtained from Figures 7.3.1-7.3.3 and that is the high concentration of extractable organics in the control sample of the artificial sea water (Instant Ocean). Typical values for extractable organics in the Atlantic Ocean are from 0.010 to 0.100 ppm, whereas the control sample of the artificial sea water contained 0.200 ppm. Qualitatively, we found a relatively high concentration of phthalates and polymers in the control samples.

(C) Outdoor experiments:

In the laboratory experiments designed to measure hydrocarbons in the water column from untreated and treated spills, the amount of oil used was just enough to give a slick of 0.05 mm thickness. However, even with dispersant only a very small fraction of the oil stayed in the water column. We felt that this was due to the small volume of water in the containers. Thus, we performed two experiments in larger test tanks using the aquarium facilities at the Narragansett Bay Campus.

Three 55 gallon fibreglassed drums were fitted with the paddle system described above to provide agitation. Each drum was filled with 190 l. of sea water on 10/26/76, and the following added:

- 1) Kuwait Crude, 155 ml (70 ppm)
- 2) Kuwait Crude/Corexit 9527, 15.5/3.1 ml
- 3) Corexit 9527, 3.1 ml

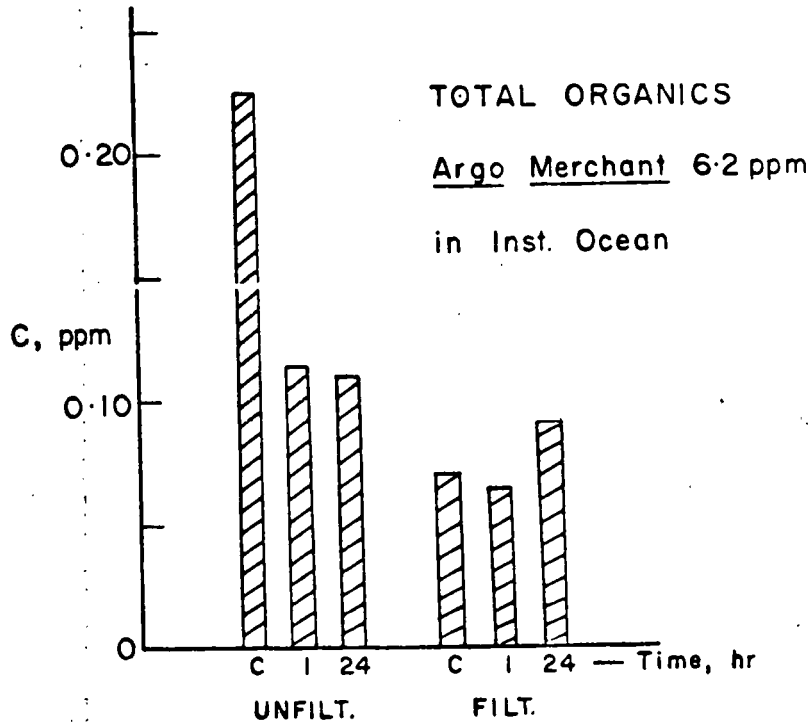


Figure 7.3.2 Total Extractable Organics from Laboratory Experiment on the No. 6 Fuel Oil from the Argo Merchant Spill.

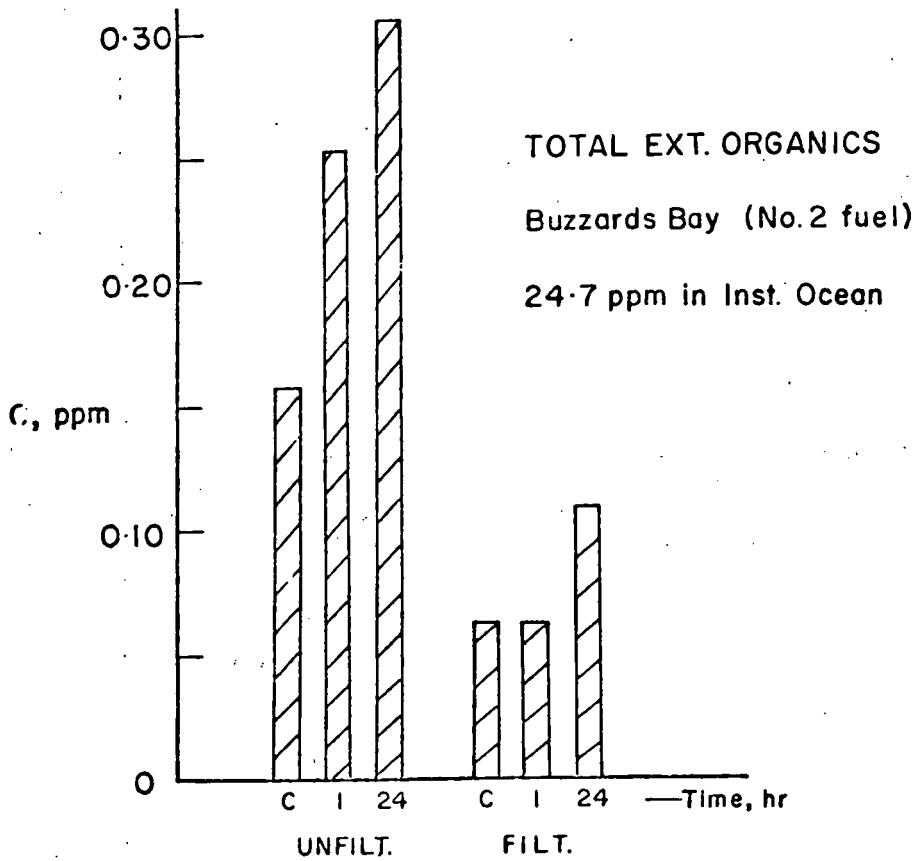


Figure 7.3.3 Total Extractable Organics from Laboratory Experiments on the No. 2 Fuel Oil from the Argo Merchant Spill

The dispersant and oil were thoroughly mixed with sea water in a 1 liter bottle prior to adding to drum #2. A 2 liter water sample was collected while filling the drums and this was used as a control. Samples (2,1) from each drum were collected at 2 and 25 hours at a depth 20 cm from the bottom. The samples were analyzed without adding an internal standard for GC analysis in order to determine the amount of internal standard needed in later experiments. Qualitative results by infrared spectroscopy indicated that an extremely small amount of oil entered the water column when the dispersant was not used.

The above experiment was repeated on 11/11/76 and all samples analyzed for total hydrocarbons, n-paraffins, other resolved components, unresolved hydrocarbons, and amount of dispersants using gas chromatography. The test tanks contained the same amount of water, oil and dispersant as the above experiment. The results of the chemical analysis are given in Table 7.3.2. The control sample contained a total of 10 g/liter of hydrocarbons. The water in the test tank having only the Kuwait Crude contained 108.4 g/liter after 2 hours, and 158.2 g/liter at 25 hours, whereas the test tank containing oil and dispersant had 646.5 g/liter after 2 hours and 20 g/liter after 25 hours. The latter value is much lower than anticipated, and we have no explanation for it at the present time.

In addition to collecting water samples, surface slick samples were also collected during experiments 1 and 2, and their infrared spectra measured. The infrared spectral fingerprints of seven samples were compared using the log-ratio method (1). In this method, the absorptivities for 18 bands in the fingerprint region are ratioed, logs of the ratios calculated and these log-ratios normalized to eliminate differences in sample thickness. Then the number of ratios within 10% of the average ratio are listed. If two samples are identical, all 18 ratios would be equal to the average; thus, the number of ratios within 10% of the average indicates the similarity between samples.

In the present case, spectra of the following samples were compared:

Kuwait = Kuwait Crude

K/D2 = Kuwait/Dispersant in H₂O column after 2 hours.

K/D24 = Kuwait/Dispersant in H₂O column after 24 hours.

Surf 1 K = Kuwait on surface after experiment 1.

Surf 2 K = Kuwait on surface after experiment 2.

Surf 1 K/D = Kuwait/Disp on surface after experiment 1.

Surf 2 K/D = Kuwait/Disp on surface after experiment 2.

The results given in Table 7.3.3 provide some useful comparisons. The fingerprints of the oil in the water column, K/D2 and K/D24, are considerably different from that of the Kuwait crude. The surface oil in the first experiment, Surf 1 K/D, is also very different from the Kuwait oil. In the first experiment, the oil, dispersant and water were

Table 7.3.2

Chemical Analysis by Gas Chromatography of
2nd Aquarium Experiment (11/11/76)

Test Tank	Time	g/liter of water				dispersant
		n-paraffins	other resolved components	unresolved envelope	total hydrocarbons	
Kuwait oil	2 hrs	6.7	16.2	85.5	108.4	—
	25 hrs	13.2	10	135	158.2	—
Kuwait Oil &	2 hrs	97.5	60	489	646.5	240*
Dispersant	25 hrs	-----			-20	320
Dispersant	2 hrs	-----			-60	300
	25 hrs	-----			-25	80
Control	0 hrs	-----			-10	—

*based on the area of the GC peak of one component; thus, the amounts listed for the the dispersants are only relative values.

Table 7.3.3

Comparison of Infrared Spectra of Kuwait, Water
Column and Surface Samples from Aquarium Experiments.

Number of ratios within 10% of average are listed.

	Kuwait	K/D ²	K/D ^a	Surf ₁ K	Surf ₁ K/D	Surf ₂ K	Surf ₂ K/D
Kuwait	18	7	3	11	5	11	11
K/D ₂		18	9	10	7	9	8
K/D ₂₄			18	6	10	8	3
Surf ₁ K				18	2	16	18
Surf ₁ K/D					18	12	7
Surf ₂ K						18	11
Surf ₂ K/D							18

^aExperiment 1; both samples were separated by TLC

thoroughly mixed in a 1 liter bottle prior to adding to the test tank. The second experiment, oil, and oil/dispersant were added to the test tanks, and then agitated with a stirring rod; thus, both surface samples compared better with the Kuwait oil.

7.3.2 Air Column

1 Charcoal Tubes

(A) Methodology

1) To analyze the air above simulated spills for hydrocarbons, the laboratory apparatus for collecting volatiles is shown in Figure 7.3.4. Initially, water is placed in the central flask and air is pumped through a charcoal filter, around the central flask, and through one of the charcoal cartridges (which becomes the control). Then oil is placed on the water in the central flask, air is pumped through the system, and the hydrocarbons are collected in the second charcoal cartridge.

After the experiment, the two charcoal canisters are extracted with CS₂. Infrared spectra and gas chromatograms of the solutions are measured; both giving qualitative and quantitative analyses.

The first set of experiments was performed on the No. 2 fuel from the Buzzards Bay spill. One hundred and fifty ml. of artificial sea water were placed in the central container and air was pumped through one of the cartridges for 1 hour; this was used as the control. Then 0.1 g of oil was added to the surface of the water and air pumped through the second cartridge for one hour. After the experiment, water from beneath the surface was extracted and analyzed. The gas chromatograms of the cargo oil, the air sample and the water sample are shown in Figure 7.3.5. For this oil, the "separation point" for the chemicals going into the atmosphere from the chemicals going into the water column is the normal paraffin n-C₁₄; the lighter molecules go into the air and the heavier into the water. Later in this report, these laboratory results are compared to the field experiments on this oil (Section 7.6).

2) Following this preliminary experiment, the more sophisticated laboratory apparatus in Figure 7.2.2 (Section 7.2.28) was constructed. When systems 1 and 2 were used, 1 ml of Kuwait crude oil was added to the surface of 150 ml. of sea water in one flask and 1.2 ml of a mixture of 5:1 (v/v) Kuwait crude oil and Corexit 9527 dispersant, were added to 150 ml of sea water in the other flask. The surface and the water were not mixed.

When system 3 was used (Fig. 7.2.6), 2 ml of Kuwait crude oil were added to the surface of 800 ml of sea water in each of the beakers, 0.4 ml of Corexit were then added dropwise to one of the beakers. The beakers were shaken immediately after the dispersant was added for a few seconds. This caused the water in the beaker containing the oil and dispersant to darken. In a few experiments, the system was continuously mixed by magnetic stirrers. Identical magnetic stirrers were used in both beakers and the stirring rate was approximately the same.

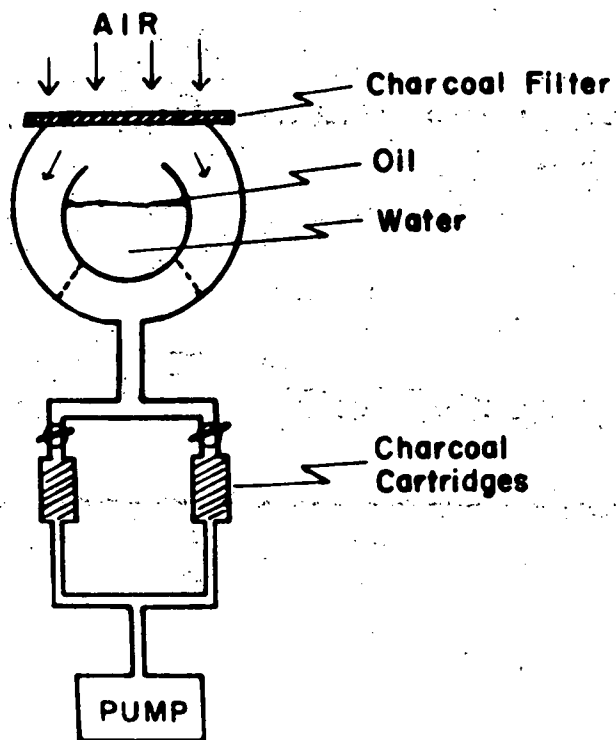


Figure 7.3.4 Laboratory Apparatus for Collecting Volatiles from Oil Slicks

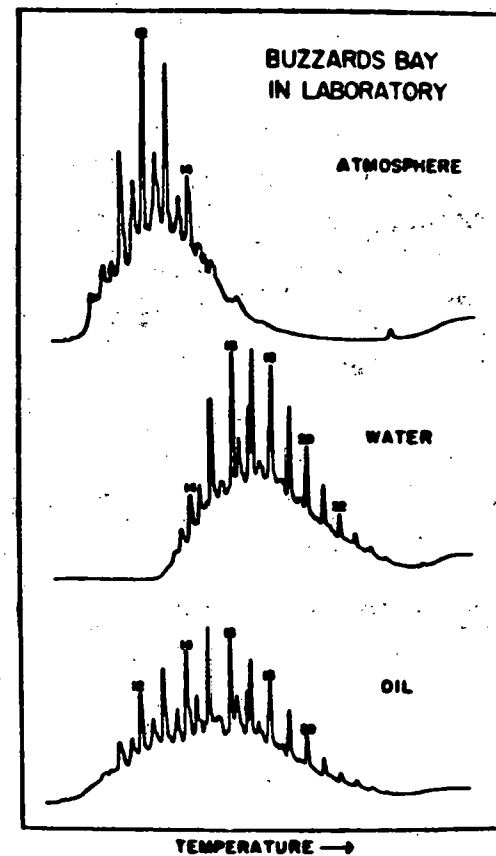


Figure 7.3.5 Gas Chromatograms from the Laboratory Experiment on the No. 2 Fuel Oil from the Buzzards Bay Spill

Air samples were taken simultaneously from both the treated and untreated slicks. In experiments when flow rates were measured, they did not differ by more than 10. Air samples were collected periodically after the spills. Experiments were conducted using 3 different flow rates of 0.2, 1.5 and 4.3 l/min.

Since air samples taken above treated and untreated spills were compared to evaluate the effects of the dispersant, it was important to determine error limits by comparing two identical oil samples. Oil was added to flasks 1 and 2 of systems A, B, and C; air samples were taken from both parts simultaneously and their gas chromatograms were compared. The results of such experiments indicate those differences which are significant when a dispersant is used. The conditions for these experiments are listed in Table 7.3.4.

Three different types of experiments were performed to determine the effects of using dispersants:

- a) Using apparatus 1 and 2, oil and oil + dispersant were added and the surface was not mixed.
- b) Using apparatus 3, oil was added and then the dispersant was added dropwise. The beakers were shaken for a few seconds after adding the oil and the dispersant.
- c) Same as 2 with continuous stirring by magnetic stirrers. Table 7.3.5 lists all experiments performed in the laboratory on evaporation of oil vs. oil + dispersant.

In experiment 6, surface samples were taken at times 1.5 and 4 hours after the spill. In experiment 11, surface samples were collected with a spatula and dried with calcium chloride. Hexane was added to deasphalt the oil. The samples were then centrifuged to remove the calcium chloride and the asphalt precipitate.

IR spectra were measured using 6 mm (pathlength) cells with silver chloride windows and teflon or stainless steel spacers. Carbon disulfide was used as a solvent for the IR measurements.

Another type of experiment was performed. A random mixture of pentane, hexane, octane, nonane, decane, dodecane, tetradecane, o-xylene, p-xylene, m-xylene, toluene and benzene was prepared. About 1 ml of the mixture was added to 150 ml of sea water and 1 ml of the mixture and 0.2 ml Corexit were added to another flask with 150 ml of sea water. Vapors were collected using apparatus A; the flow rate was about 0.2 l/min and the water was not mixed. The same experiment was performed using apparatus B and the flasks were shaken after adding the mixtures. A flow rate of 3.4 liters/min was used for this experiment.

(B) Experimental Results

(i) Oil vs. oil on water-evaporation experiments

Experiments 1-5, as mentioned in the above section, were performed in order to find the experimental errors of systems 1, 2, and 3 and to

Table 7.3.4

Flow Rates and Sample Times for Laboratory Experiments 1-5

Exp #	Water Temp. OC	Time Taken	System	Flow Rates	
				oil 1	oil 2
1	19	0-0.5	A	1.56	1.56
		0.5-1.5	A	1.44	1.40
		1.5-4	A	1.24	1.40
2	19	0.5-1.5	B	1.56	1.56
3	19	0-0.5	B	1.52	1.52
		0.5-1.5	B	1.56	1.56
4	18	0-0.5	C	2.00	2.10
		0.5-1.5	C	1.76	1.84
5	18	0-0.5	C	4.30	4.30
		0.5-1.5	C	4.30	4.30

Remarks:

Time - hours after the spill.

Flow rates are in lit/min.

In experiment 2, did not pump during 0-0.5 hours.

In experiment 4, distance between funnel and beaker 2.5 cm.

In experiment 5, distance between funnel and beaker 1.5 cm.

and there was 1200 ml sea water in the beakers.

Table 7.3.5
Flow Rates and Sample Times for Laboratory Experiments 6-16

P	Water Temp. oC	Time Taken	System	Flow Rate		Mixing
				oil	oil/disp	
6	20	0-1.5	A	< 0.2	< 0.2	no
		1.5-4	A	< 0.2	< 0.2	
7	20	0-1.5	A	< 0.2	< 0.2	no
		0.5-4	A	< 0.2	< 0.2	
8	20	0-1.5	A	< 0.2	< 0.2	no
		1.5-4	A	< 0.2	< 0.2	
9	20	0-1.5	A	< 0.2	< 0.2	no
		1.5-4	A	< 0.2	< 0.2	
10	17	0-0.5	A	< 0.2	< 0.2	no
		0.5-1.5	A	< 0.2	< 0.2	
		1.5-4	A	< 0.2	< 0.2	
		4-7	A	< 0.2	< 0.2	
		7-12	A	< 0.2	< 0.2	
		12-23	A	< 0.2	< 0.2	
		23-31	A	< 0.2	< 0.2	
11	17	0-0.5	A	1.44	1.44	no
		0.5-1.5	A	1.44	1.44	
		1.5-4	A	1.36	1.24	
		4-7	A	1.56	1.56	
		7-12	A	1.44	1.56	
		12-24.5	A	1.52	1.52	
		24-5-31	A	1.52	1.52	
12	16	0-0.5	B	4.24	4.28	no
		0.5-1.5	B	4.04	4.32	
		1.5-4	B	4.28	4.04	
13	16	0-0.5	C	1.60	1.60	yes
		0.5-1.5	C	1.60	1.60	
		1.5-4	C	1.60	1.60	
		4-7	C	1.60	1.60	
		7-23.25	C	1.60	1.60	
14	15	23.25-29	C	1.60	1.60	yes
		0-0.5	C	1.60	1.60	
		0.5-1.5	C	1.60	1.60	
15	18	1.5-4	C	1.60	1.60	const.
		0-0.5	C	1.60	1.60	
		0.5-1.5	C	1.60	1.60	
16	18	1.5-4	C	1.60	1.60	const.
		0-0.5	C	1.60	1.60	
		0.5-1.5	C	1.60	1.60	
		1.5-4	C	1.60	1.60	

Remarks:

Flow rates are in lit/min.

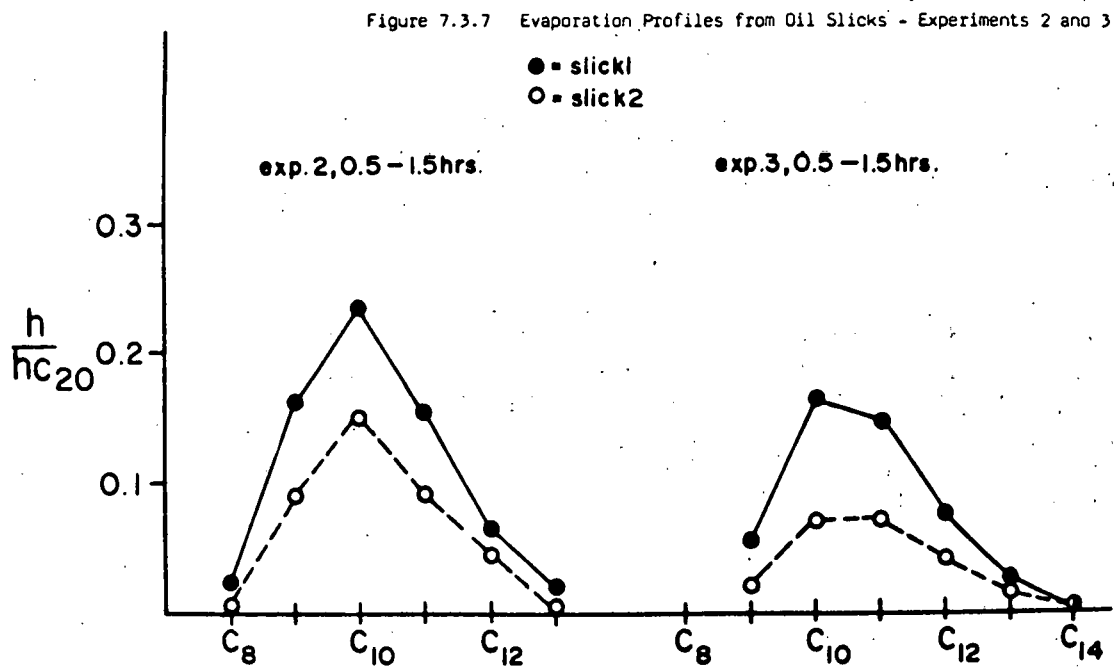
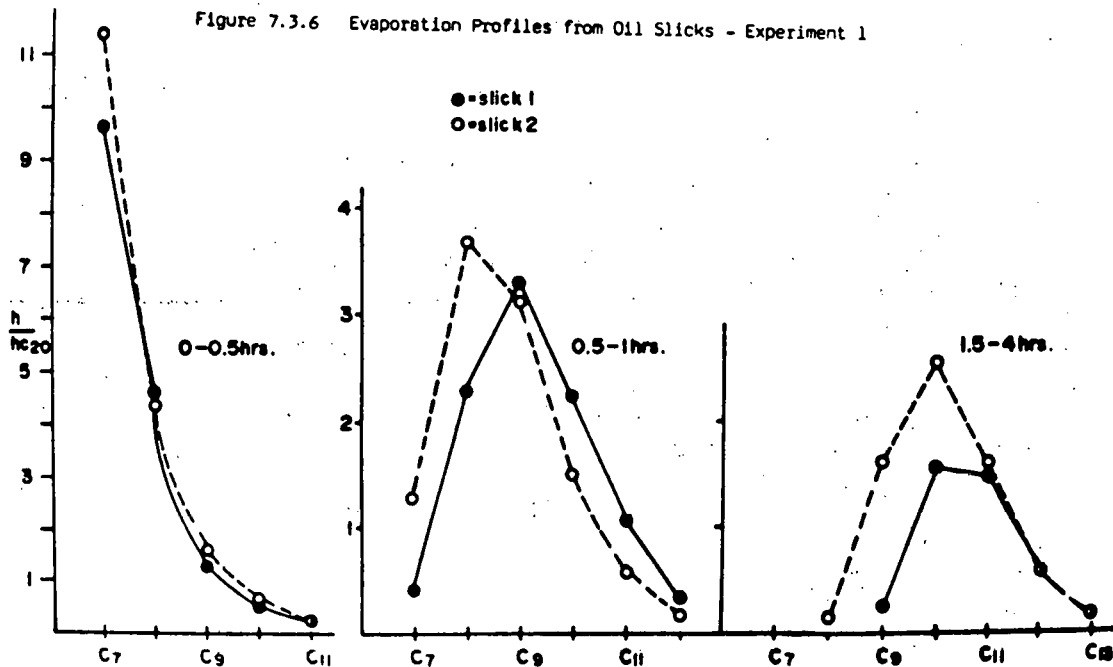
Time is in hours after the spill.

Const. = constant mixing during the entire experiment.

determine if differences between the evaporation of oil and oil + dispersant slicks are due to the dispersant or to the experimental conditions and procedures. When both parts of the system contained only oil, differences in the evaporation rates could be caused by differences in flow rates, or differences in the crude filters used in system A. Since only the GC peaks of the normal alkanes were definitely identified and their GC peaks are the most intense, they were used to compare the two samples. Each sample, i.e., the one taken above part 1 and the one taken above part 2, contained the same amount of internal standard ($n\text{-C}_{20}$). The relative heights of the GC peaks of each normal alkane to the height of $n\text{-C}_{20}$ were calculated and plotted as a function of the carbon number of that certain n -alkane. The plots for experiment No. 1 for the samples collected during 0-0.5, 0.5-1.5 and 1.5-4 hrs. after the oil addition are shown in Figure 7.3.6. The evaporation rates of oil components from the slick were ordered according to their vapor pressures, i.e., heptane, octane, etc. Usually after 0.5 hrs., these graphs have maxima which change with time towards the heavier n -alkanes. For example, in experiment 1 (slick 1) the sample taken during 0.5-1.5 hrs. had a maximum at $n\text{-C}_9$, whereas in the sample taken at 1.5-4 hrs. the maximum moved to $n\text{-C}_{10}$.

The ratio HC_x/HC_{20} ($x=7,8,\dots$), where HC_x is the GC peak height of a normal alkane with x carbons and HC_{20} is the GC peak height of $n\text{-C}_{20}$, is proportional to the amount of $n\text{-C}_x$ that evaporated. This ratio for a particular n -alkane in two air samples taken under the same conditions can be compared, i.e., the ratio HC_8/HC_{20} in air samples taken during the same time and in the same experiment above slick 1 and slick 2. This comparison was justified since the collection efficiency, extraction efficiency, detector response, GC conditions (temperature and flow rate) and the amount of standard added to both samples were the same. The envelope formed by these plots indicates when a certain n -alkane starts to evaporate and when its evaporation process is over. The differences in the shape of the envelopes of two samples taken during the same time and conditions indicate differences in the evaporation process of the light components from the slick. For experiments 1-5, the more similar the shapes of the envelopes of the two samples taken simultaneously, the better, i.e., it means that the system is good for determining the effects of dispersants on the evaporation.

Figure 7.3.6 shows the envelopes obtained for experiment 1. When system A was used, there was a difference in the position of the maximum in the samples of 0.5-1.5 and 1.5-4 hrs. The evaporation rates of the two identical slicks were different. Slick No. 1 had a faster rate. It could be that the crude filters were not exactly identical and have caused the differences. Experiments 2 and 3 were performed using apparatus B which is similar to apparatus A, with the filters removed. Results of these experiments are illustrated in Figure 7.3.7. The envelopes obtained for slicks 1 and 2 at 0.5-1.5 had the same shape. The evaporation process was faster when the filters were removed and the maximum of the envelope was at $n\text{-C}_{10}$ for both slicks in experiments 2 and 3, whereas in experiment 1, it was at $n\text{-C}_8$ for slick 2 and at $n\text{-C}_9$ for slick 1. Collection efficiency decreased from experiment 1 to experiments 2 and 3. This could be due to the removal of the filters. When they covered the apparatus, they could have interfered in the escape of vapors into the room atmosphere, so less was lost and more was collected;



this could also be the reason for the slower evaporation rate.

The results of experiments 1, 2 and 3 indicated that another system should be tried in which more sea water and more oil would be used. This would ensure that the air samples would be concentrated enough without having to interfere in the natural evaporation process, e.g., partially closing the system. System C seemed to fulfill those requirements. Figure 7.3.8 shows the results obtained when apparatus C was used (experiment 4). There is a slight difference between the two envelopes in the relative amounts of n-C₁₀ and n-C₁₁ (less than 10). Experiment 5 was the same as experiment 4 except for the flow rate that was higher and the distance between the oil slicks and the funnels, which was smaller in experiment 5. Results are illustrated in Figure 7.3.9; samples were too concentrated and the evaporation rate was slower than in experiment 4, possibly because the funnels were too close to the oil surface. Differences between the two envelopes were in the same order as in experiment 4.

(ii) Oil vs. oil + dispersant evaporation experiments

a) Experiments with no mixing of the surface:

Laboratory experiments 6-9 were performed under identical conditions. Samples were taken at 0-1.5 and 1.5-4 hrs. after adding the oil and oil + dispersant using system 1. The n-alkane GC peaks were identified by retention time. Toluene, p-xylene, m-xylene, and o-xylene GC peaks were also identified by retention time and, furthermore, their GC effluents were collected and IR spectra measured. The IR spectra showed that their peaks contained an additional component, which was probably a branched alkane. The benzene peak was identified by retention time and by the appearance of the benzene band at 670 cm⁻¹ in the IR spectrum of the mixture. For air samples collected at 0-1.5 hrs., the following ratios of the GC peak heights were calculated: benzene/octane, toluene/nonane and p-xylene + m-xylene/nonane. Table 7.3.6 lists the values obtained.

From the values shown in Table 7.3.6, it can be observed that the corresponding ratios are bigger in the oil + dispersant sample than in the oil sample. This could mean that there was less octane and nonane evaporating from the treated slick than from the untreated slick, or that more of the benzenes were evaporating from the untreated slick. This could be caused by the dispersant mixing more aliphatic than aromatic hydrocarbons into the water column. Decane was not taken into consideration in the calculations as its corresponding GC peak was small and it also contained o-xylene.

Figure 7.3.10 shows the gas chromatograms of the air samples above the treated and untreated oil spills taken at 0-1.5 hrs.

It was interesting to see whether this phenomenon also occurred when mixing was applied; thus, experiments 15 and 16 were performed with constant mixing. When calculating the above mentioned ratios for samples taken at 0-0.5 hrs., the trend found in experiments 6-9 was not observed. When mixing was applied, the dispersant affected the light and the heavy hydrocarbons differently, whereas without mixing the dispersant

Figure 7.3.8 Evaporation Profiles from Oil Slicks - Experiment 4

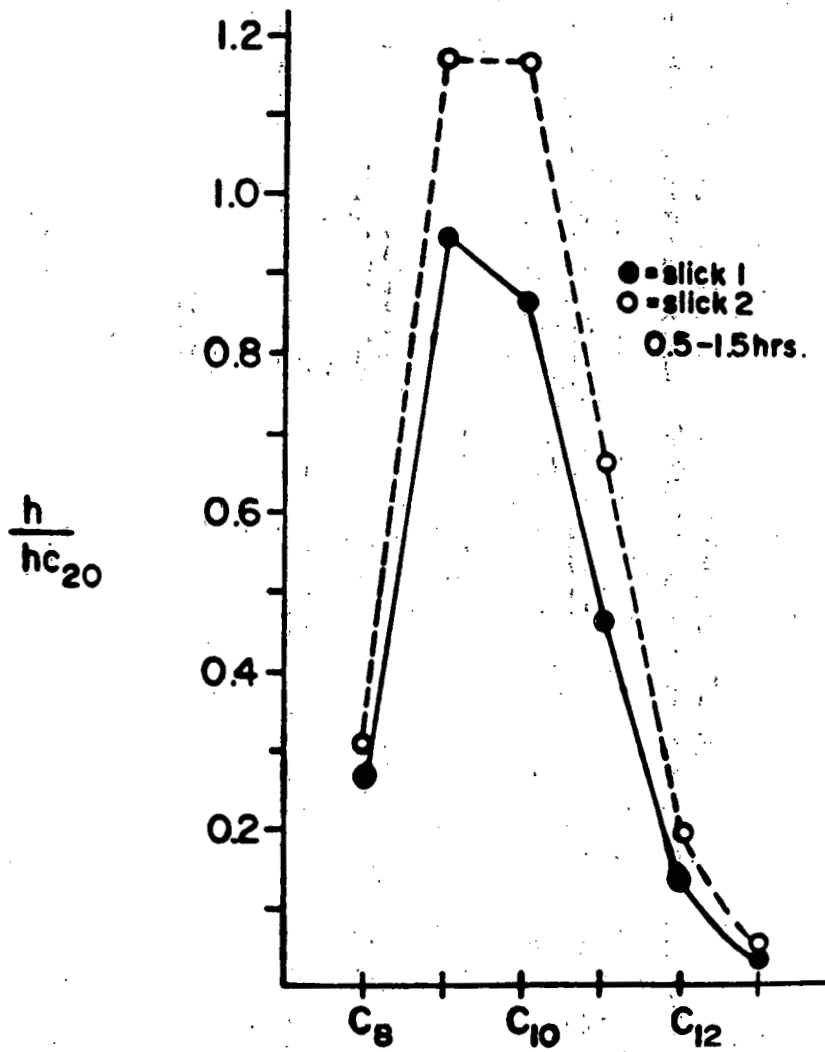


Figure 7.3.9 Evaporation Profiles from Oil Slicks - Experiment 5

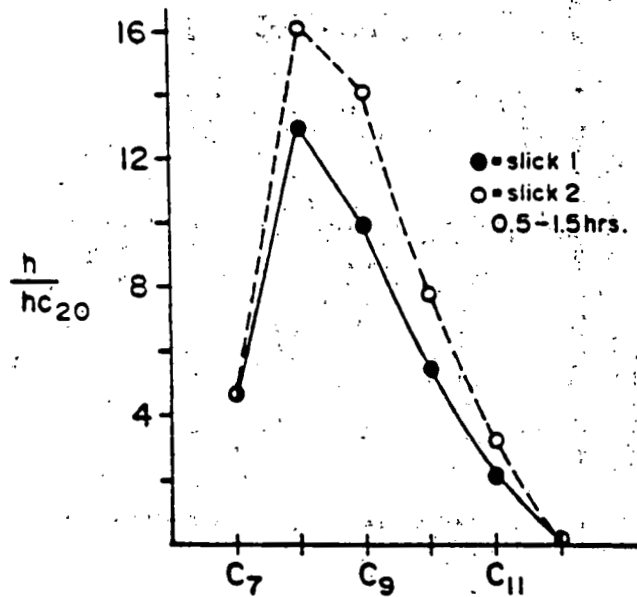


Figure 7.3.10 GC of Air Samples at 0-1.5 Hours

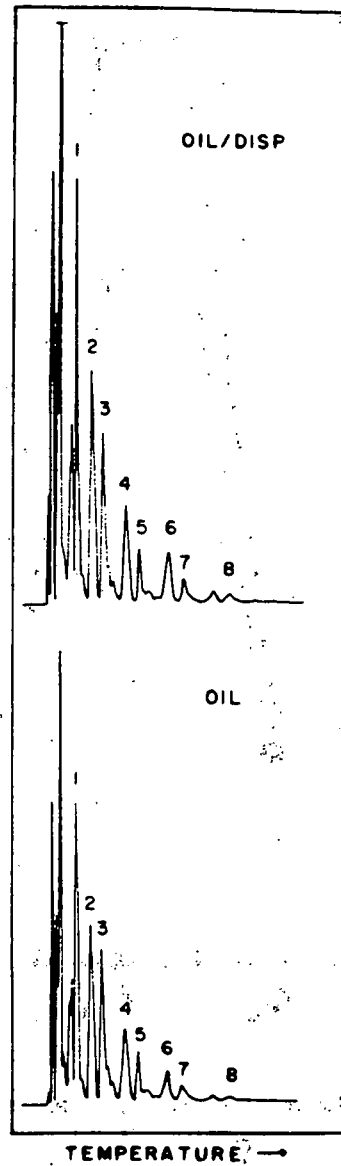


TABLE 7.3.6
 Ratios of GC Peak Heights for Experiments 6-9

	Exp 6		Exp 7		Exp 8		Exp 9	
	Oil	Oil/Disp	Oil	Oil/Disp	Oil	Oil/Disp	Oil	Oil/Disp
ben/oct	1.16	1.35	1.17	1.37	1.07	1.54	1.11	1.25
tol/non	1.36	1.70	1.54	2.00	1.37	2.50	1.29	1.35
m-xy/non	0.63	0.93	0.65	0.82	0.64	1.12	0.67	0.79

ben = benzene

tol = toluene

non = nonane

oct = octane

o,m-xy = p-xylene + m-xylene

affected aromatics and aliphatics differently. This is illustrated in Table 7.3.7 which shows the ratios of corresponding peak heights in the two gas chromatograms obtained from air samples in experiment 15. The order of the compounds in Table 7.3.7 is the order in which their peaks appear on the gas chromatogram. If relative amounts of those components were the same in both samples, those ratios should have been constant; however, they increase from the lighter components toward the heavier ones, indicating that relatively less of the light ones, such as heptane, benzene and octane, evaporated from the treated slick.

The chromatogram of the samples taken at 1.5-4 for experiment 6-9, Figure 7.3.11, show that the evaporation was faster for the oil slick. The n-C₇ peak was very small in the oil sample and n-C₉ was the strongest peak. In the oil + dispersant sample, n-C₇ was relatively more intense and n-C₈ peak was almost as high as the n-C₉ peak. Surface samples taken in experiment 6 at 1.5 and 4 hrs. after the spills indicated the same results, i.e., the oil slick evaporated faster. After 4 hrs., n-C₈ was gone from the oil slick, but it still appeared in the oil + dispersant slick. Slight mixing might have been performed when the surface samples were collected and when charcoal tubes were changed.

In order to obtain more conclusive data about the effect of the dispersant on aromatic and aliphatic hydrocarbons, a known mixture of light aromatics and aliphatic hydrocarbons was investigated. When no mixing energy was applied there was no significant difference between the relative heights of the n-alkanes and benzene with and without dispersant. When mixing was applied, there were differences; the amount collected above the mixture was larger than the amount collected above the mixture/dispersant. The relative amounts of benzene, octane, n-C₁₂ and n-C₁₄ in the mixture/dispersant were higher than in the mixture only. Relative amounts of Toluene, p-xylene + m-xylene and decane + o-xylene were the same in both samples. Table 7.3.8 shows the ratios of the peak heights in both samples. These results suggest that the dispersant has different effects on light hydrocarbons than on heavier ones without regarding aromatic character but, as this is a simple mixture and not oil, it may be inaccurate to apply results from one system to the other.

In experiment 10 and 11, air samples were taken over 30 hrs. so that evaporation rates of heavier hydrocarbons could be obtained. Experiments 10 and 11 were the same except for the flow rate of the pump, which was higher in experiment 11. Evaporation rates of each of the n-alkane can be obtained by plotting the total amount collected during time x as a function of time. The total amount of a certain n-alkane collected up to a certain time is proportional to the sum of HC_x/HC₂₀ in the air samples taken up to that time. For example, the total amount of n-C₈ that was collected during 4 hrs. will be proportional to: (HC₈/HC₂₀) 0-0.5 + (HC₈/HC₂₀) 0.5-1.5 + (HC₈/HC₂₀) 1.5-4. This is correct only if the same amount of standard was added to all samples. Since the collection efficiency is unknown, the proportionality constant between the total amount evaporating and the sum of the relative height cannot be calculated, but plotting that sum as a function of time will be sufficient to show evaporation rates.

Table 7.3.7 Ratio of Corresponding Peak Heights - Experiment 15

hep	R-ben	R-oct	R-tol	R-non	R-p,m-xy	R-o-xy+dec
8	0.91	0.92	1.3	1.34	1.57	2.3

Is the ratio of the GC peak height of x in the oil/dispersant sample the GC peak height of x in the oil sample.

h = heptane

b = benzene

o = octane

n = nonane

t = toluene

m-xy = p-xylene + m-xylene

xy+dec = o-xylene + decane

Table 7.3.8 Ratio of GC heights for Both Samples

R-oen	R-oct	R-tol	R-non	R-p,m-xyl	R-o-xyl+dec	R-dode
1.02	1.21	1.71	1.69	1.72	1.76	0.47

Is the ratio of the GC peak height of x in the mixture sample to the peak height of x in the mixture/dispersant sample.

ben = benzene

oct - octane

tol - toluene

non = nonane

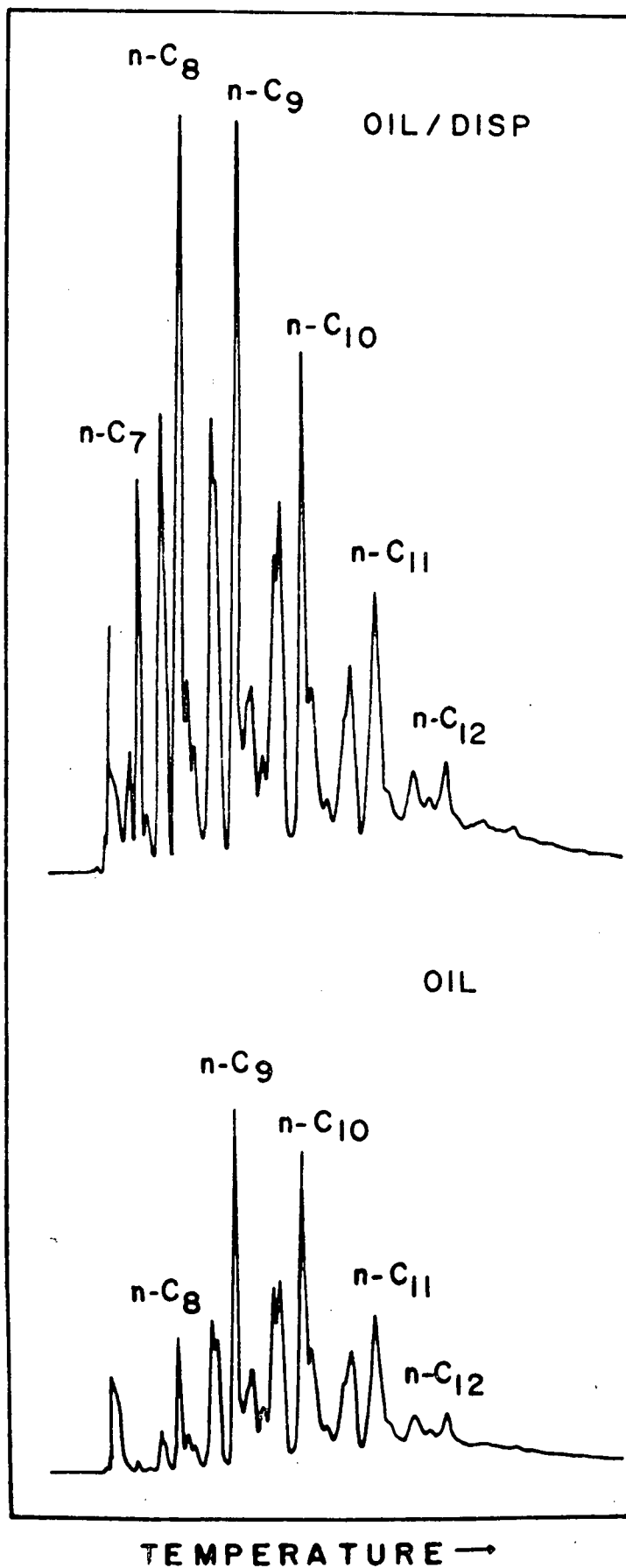
p,m-xyl = p-xylene + m-xylene

o-xyl+dec = o-xylene + decane

dode = dodecane

tetd = tetradecane

Figure 7.3.11 GC of Air Samples at 1.5-4 Hours - Experiments 6-9



Figures 7.3.12, 7.3.13, and 7.3.14 show the envelopes obtained for experiment 10. Comparison to experiment 1 indicates that the small differences in the evaporation rates of the oil slick and the oil + dispersant slick is insignificant and that they actually behaved similarly. Figure 7.3.15, 7.3.16, and 7.3.17 show the evaporation rates of n-C₇ to n-C₁₄; again the n-alkanes of both slicks evaporated at about the same rates.

The total amount of vapors collected is proportional to the relative areas of the whole chromatogram of the air sample (not including n-C₂₀) to the n-C₁₀ peak area. By plotting the total relative area as a function of time, total evaporation rate of the slick can be obtained. Figure 7.3.18 shows the evaporation rate of the slicks for experiment 10. The slight difference between the oil and the oil + dispersant slicks is meaningless and the evaporation rates can be considered the same.

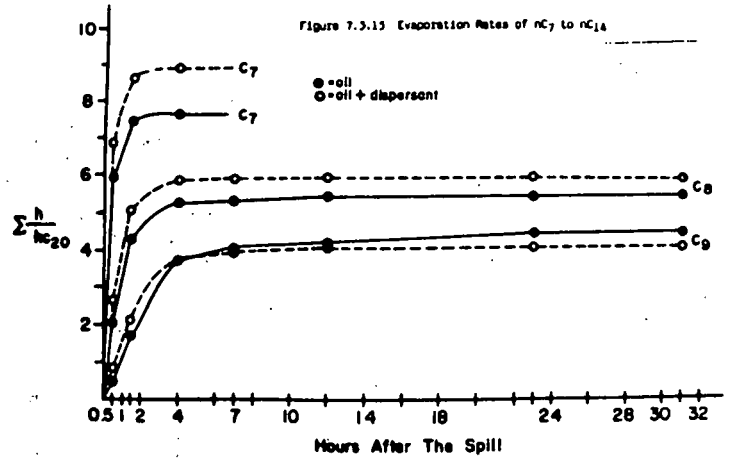
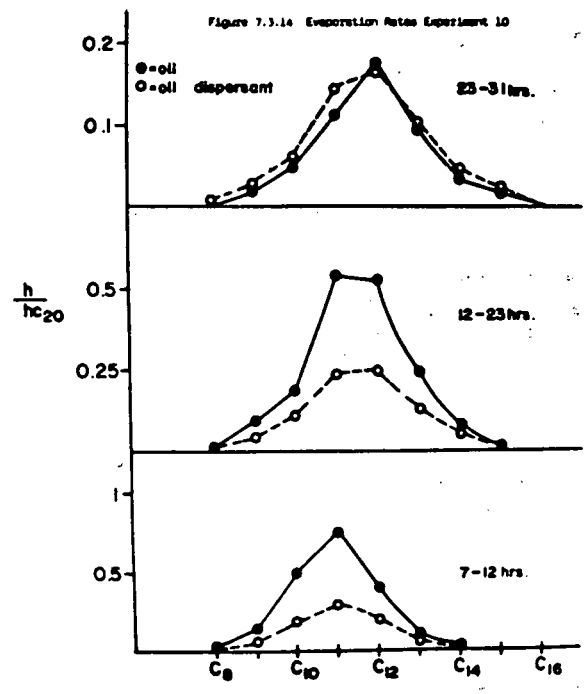
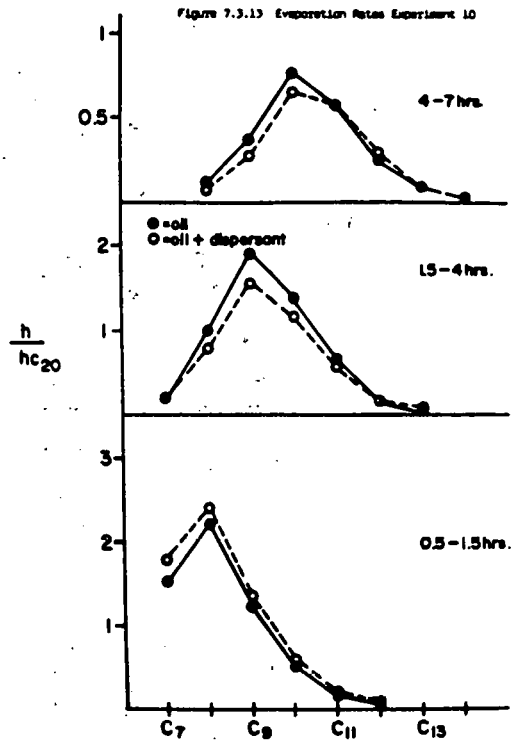
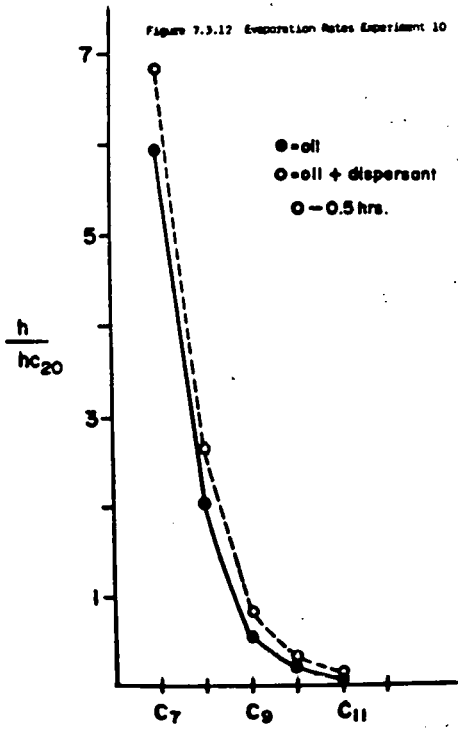
When looking at the envelopes (Figure 7.3.19, 20 and 21 obtained for experiment 11, and at the evaporation rates of the individual n-alkanes (Figure 7.3.22, 23 and 24) it can be concluded that the evaporation process is faster in the oil slick than in the oil + dispersant slick. When comparing the difference to the results of experiment 1, it is really difficult to say whether the differences were due to the dispersant or not, since they were very much like the differences occurring in experiment 1. Figure 7.3.25 shows that the total evaporation rates of the slicks were similar.

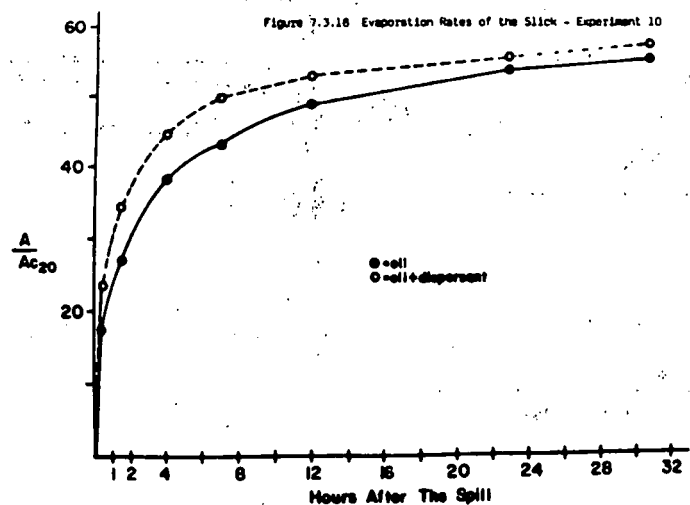
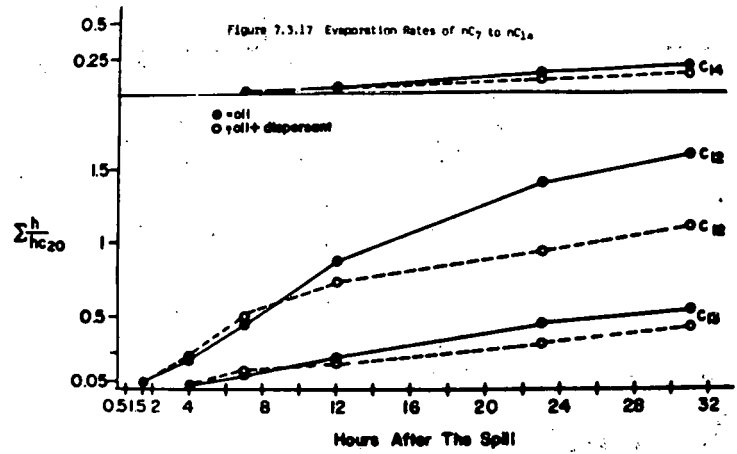
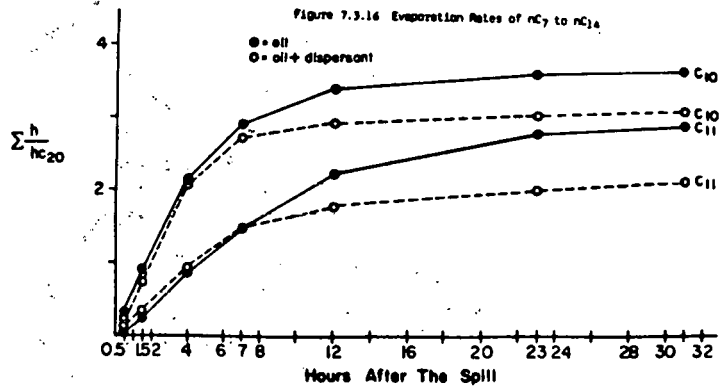
Since the only difference in the experimental conditions in experiments 10 and 11 was the pump flow rate, it could be assumed that the oil slick is affected to a greater extent from the pumping rate than the oil + dispersant slick. Experiment 12 was performed to verify this. Since the crude filters could cause differences, they were removed (system B used) and the pump flow rate was increased by a factor of almost 3. Samples in experiment 12 were taken only up to 4 hrs.; this was enough to determine the rate of evaporation and the differences between the treated and untreated slicks. This experiment gave very close results for the n-alkanes evaporating from both slicks as illustrated in Figures 7.3.26 and 27. Therefore, the flow rate does not affect the oil slick by causing it to evaporate faster.

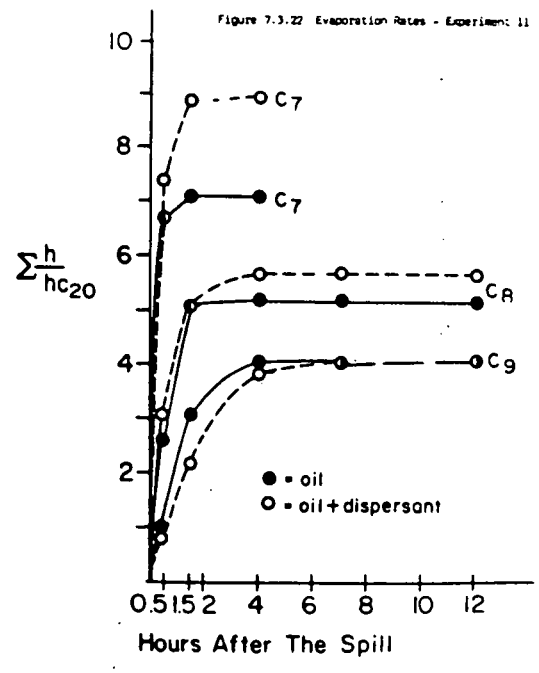
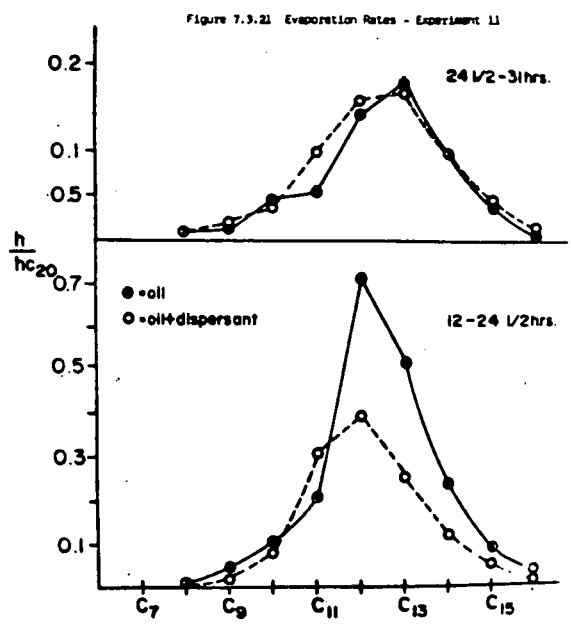
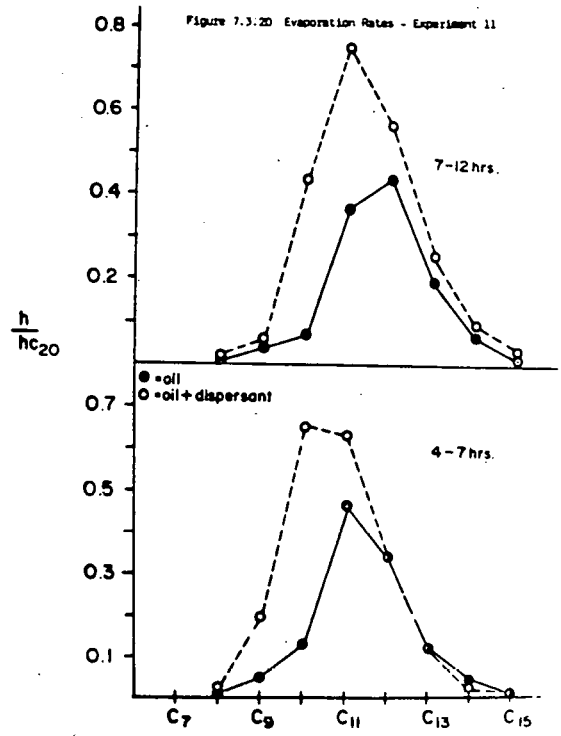
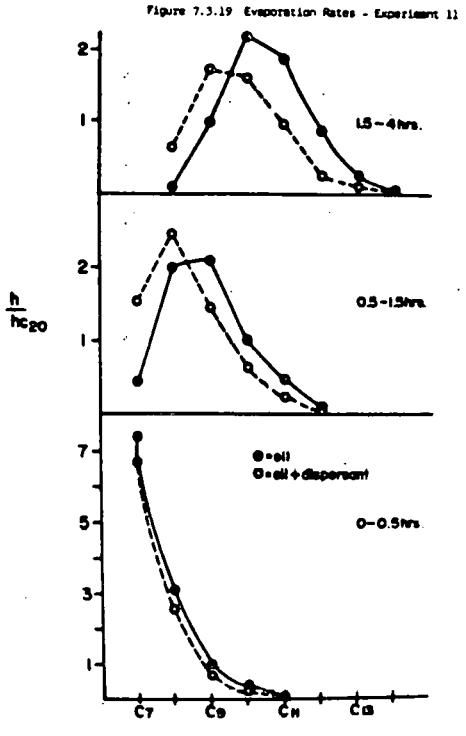
Experiments 6 to 12, which were all performed without mixing, did not show a constant trend; evaporation was either the same or the untreated slick evaporated slightly faster. However, the difference was not much larger than in experiment 1 (oil vs. oil, using system A). When the surface was not mixed, the dispersant did not have a significant effect on the evaporation of the n-alkanes.

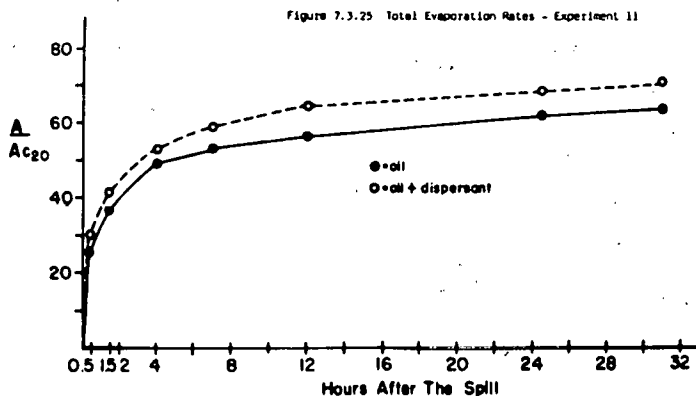
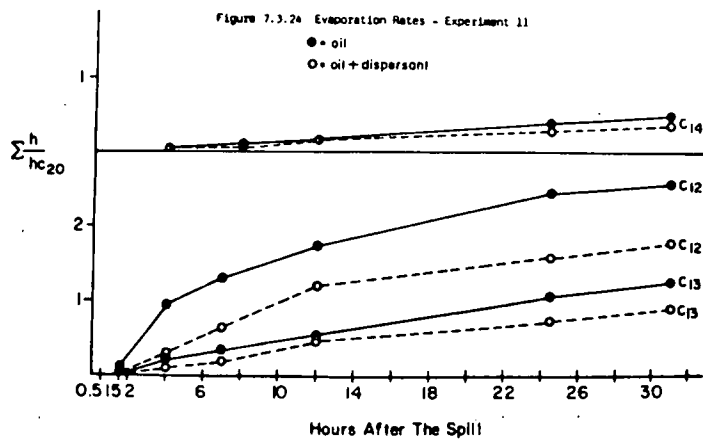
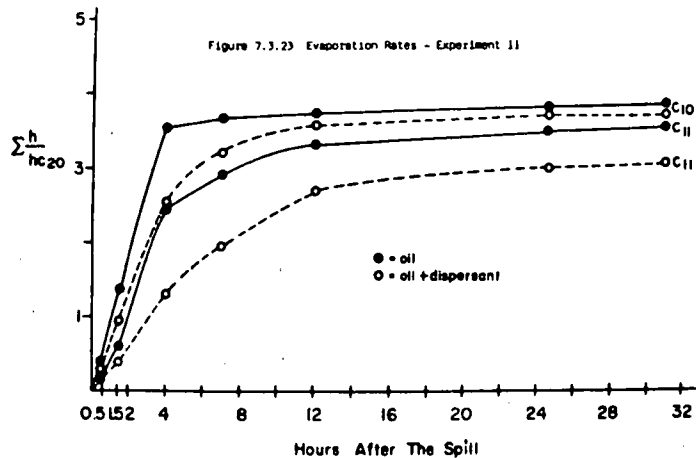
b) Experiments with mixing directly after the spill

In the case of an oil spill in the open sea, there is mixing of the surface slick into the water column by waves; thus, it is necessary to determine the effect of mixing on the dispersant. Experiments 13 and 14 were performed using system C. The oil was first added to both beakers and the dispersant was then added to one of them and both beakers were shaken for a few seconds. After shaking the beakers, the water in the









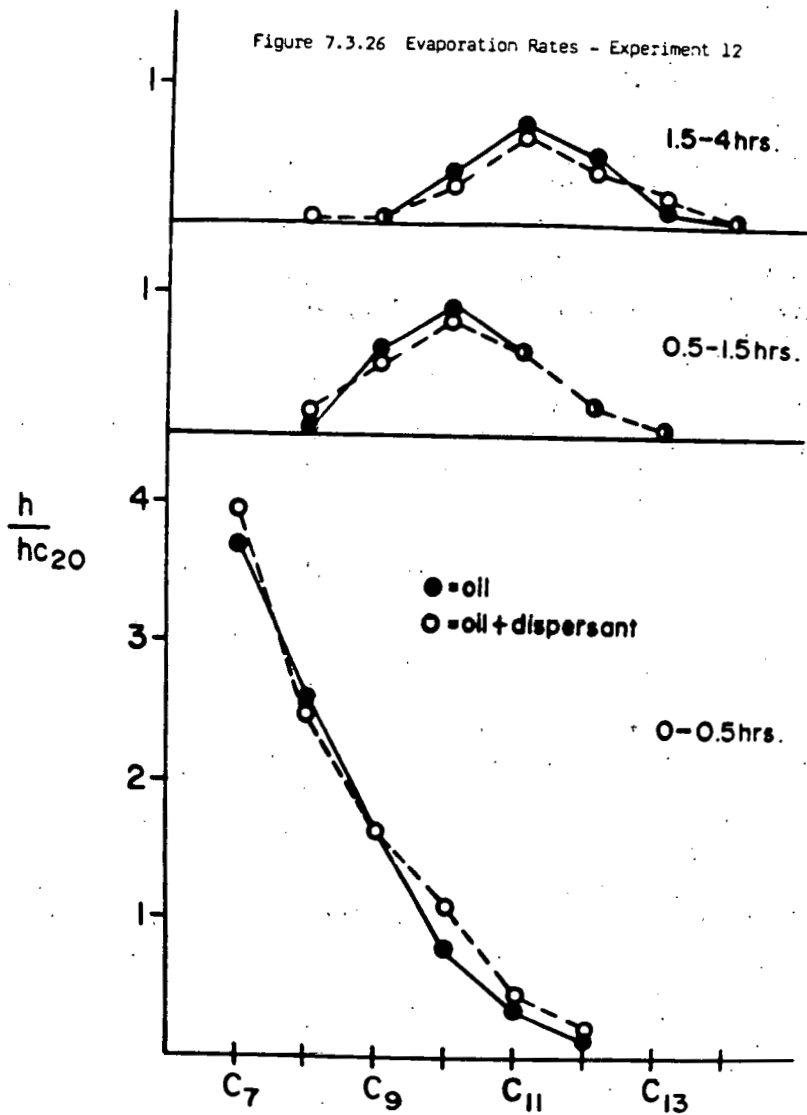
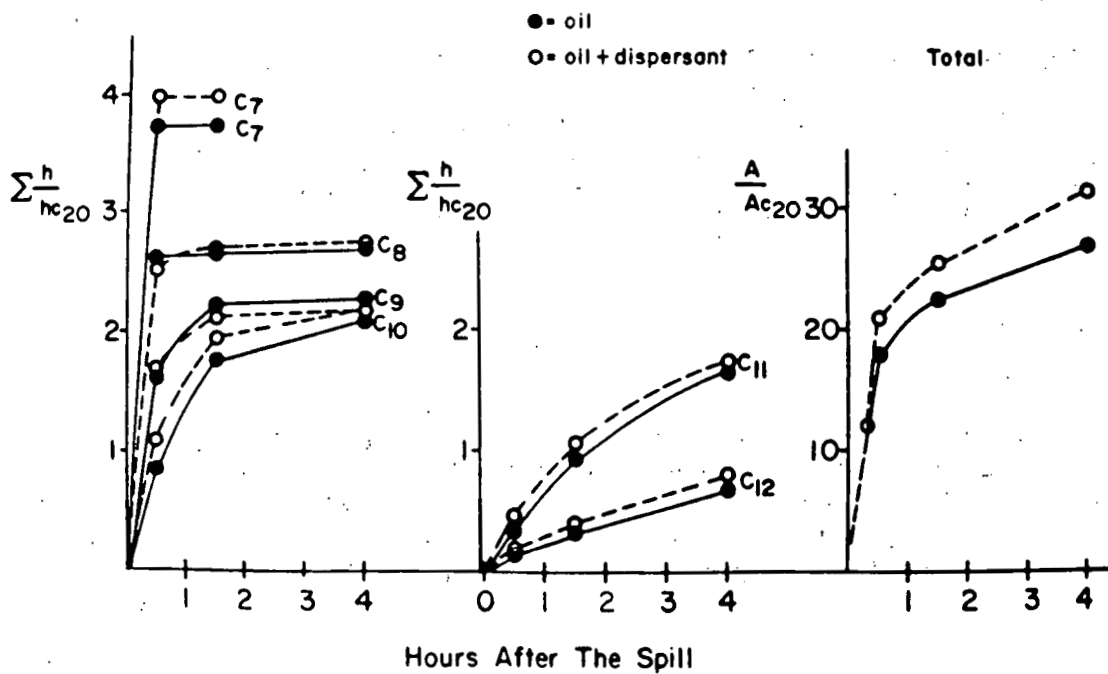


Figure 7.3.27 Evaporation Rates - Experiment 12



oil only beaker remained clear, whereas the water in the oil + dispersant beaker became dark. However, the color gradually became lighter indicating that some of the oil originally in the water was returned to the surface. Mixing made the dispersant more effective and the evaporation rate of the n-alkanes from the treated slick was slower than from the untreated slick. The difference was larger than could have been caused by experimental errors as indicated in experiment 4. Figures 7.3.28 and 7.3.29 show the difference in the relative heights of the n-alkanes as a function of the carbon number. n-C₇ showed up in the air sample taken above the treated slick during 1.5-4 hrs., whereas n-C₈ was very weak and n-C₇ disappeared from the corresponding air sample taken above the untreated slick. The heavier components such as n-C₁₂, n-C₁₃, n-C₁₄ and n-C₁₅ started to appear in both samples at about the same time, but it took much longer for the light ones, n-C₇ to n-C₁₀ to evaporate from the treated spill as indicated by Figures 7.3.30 and 31.

c) Experiments with constant mixing during the entire experiment.

In experiments 13 and 14, mixing was applied only at the beginning of the experiment; the effects of a dispersant will probably be even greater when there is constant mixing throughout the experiment. Experiments 15 and 16 were performed with constant mixing. At the beginning of the experiment, the beakers were shaken and then the water was stirred with magnetic stirrers. This kept the water of the treated spill dark while the water of the untreated spill was clear with only a few drops of oil sinking to the bottom of the beaker and rising to the surface. In these experiments, there was a big difference between the evaporation of the two slicks; the oil + dispersant air samples did not show a normal envelope, but one that had a flat maximum and a minimum as is shown in Figures 7.3.32 and 33. Evaporation was much slower for the treated spill, n-C₇ was still coming off the treated slick after four hours, whereas, n-C₈ was gone from the untreated slick. The heavier n-alkanes such as n-C₁₂ to n-C₁₅ showed up at about the same time from both slicks. In the untreated slick, the order in which the components evaporated seemed different from the order expected from vapor pressures. Figures 7.3.34 and 35 show the evaporation rates of n-C₇ to n-C₁₂. The largest differences are found in the lighter components.

Surface samples of the slicks were taken at 7 hrs. after the spill. Their chromatograms are shown in Figures 7.3.36. In the oil slick, all components lighter than n-C₁₁ had already evaporated but in the oil + dispersant slick sample, all components heavier than n-C₈ appeared. The data obtained from the surface are samples were in agreement with those obtained from the oil samples; evaporation was faster from the untreated slick.

(C) Conclusions:

The laboratory study using the self-mixing dispersant Corexit 9527, indicated the evaporation of the n-alkanes from the treated and untreated slicks was similar when the water was not agitated. However, when mixing was applied, the effects of the dispersant on the evaporation became significant. The evaporation of the light n-alkanes, n-C₇ to n-C₁₀, from the treated slick was slower than from the untreated slick. The longer the mixing, the greater was the effect of the dispersant on the

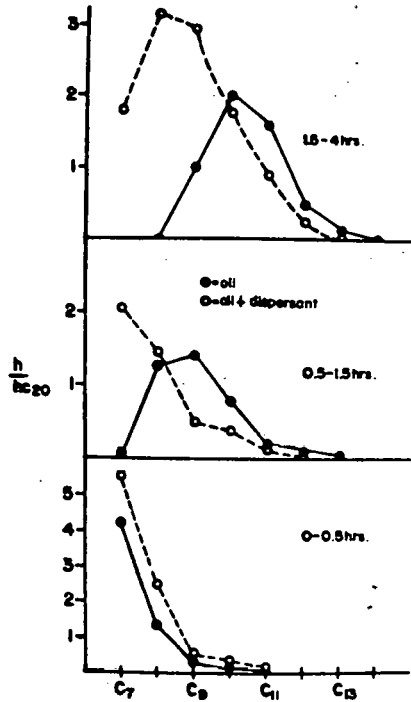


Figure 7.3.28 Relative GC Peak Heights of the n-alkanes as a function of the carbon number: C₇, C₉, C₁₁, C₁₃, 0.5 - 1.5 hrs.

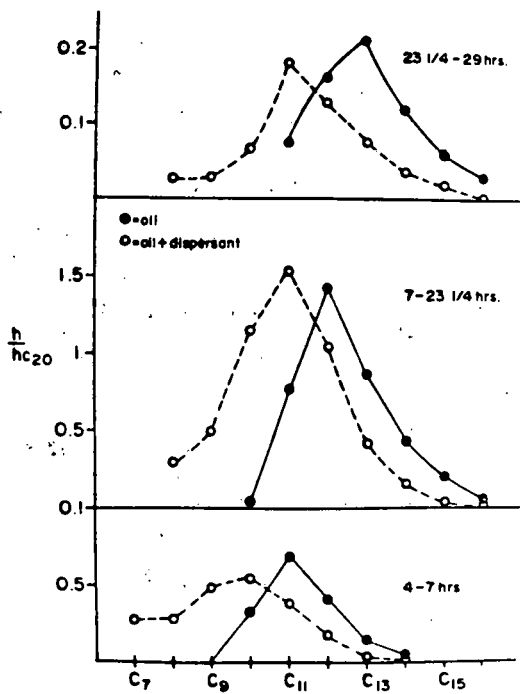


Figure 7.3.29 Relative GC Peak Heights of the n-alkanes as a function of the carbon number: C₇, C₉, C₁₁, C₁₃, 7-23 1/4 hrs.

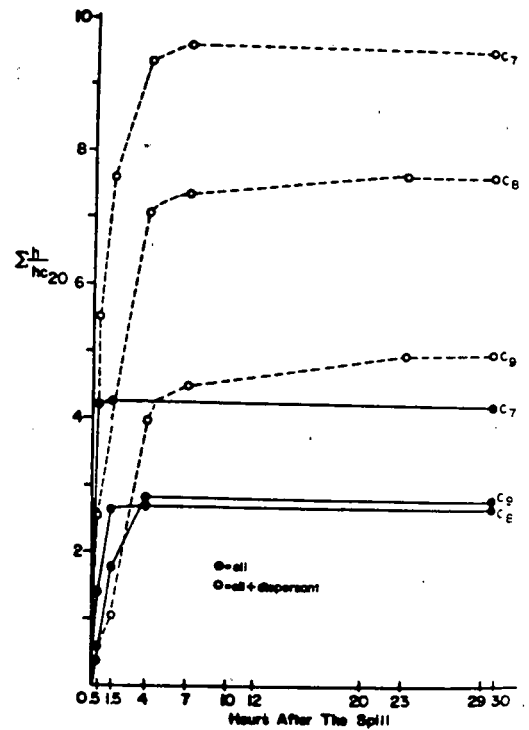


Figure 7.3.30 Evaporation Rates of n-C₇, n-C₈ and n-C₉ Experiments 13 and 14

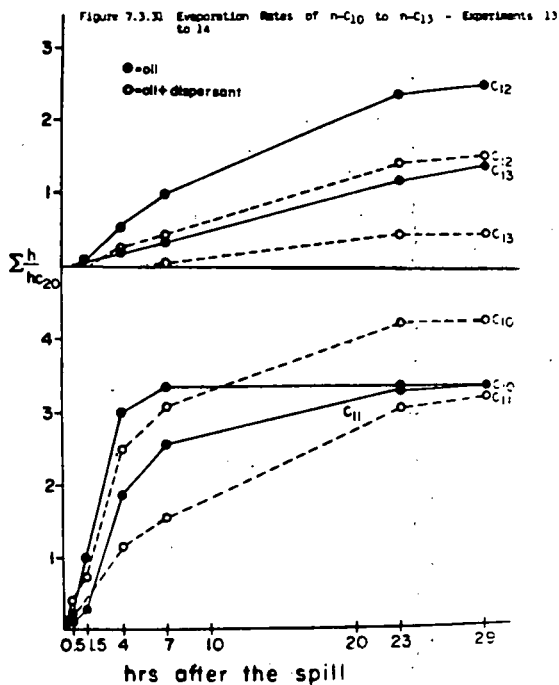


Figure 7.3.32 Relative GC Peak Heights of the n-alkanes as a function of the carbon number. Air Samples, Experiments 13 and 14.

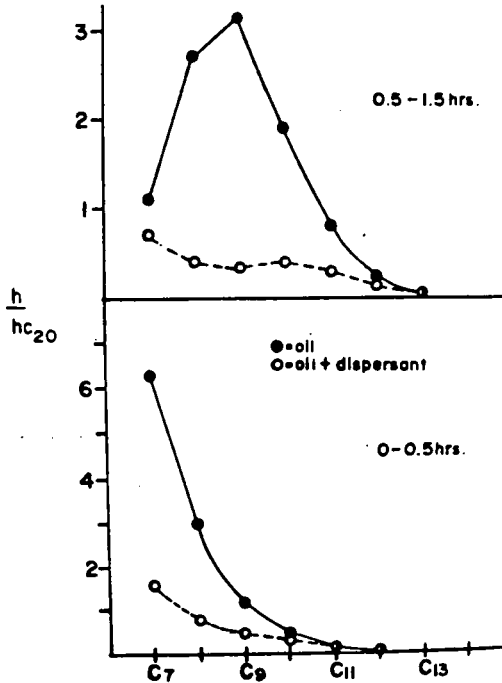


Figure 7.3.33 Relative GC peak heights of the n-alkanes as a function of the carbon number. Air Samples Exp. 16

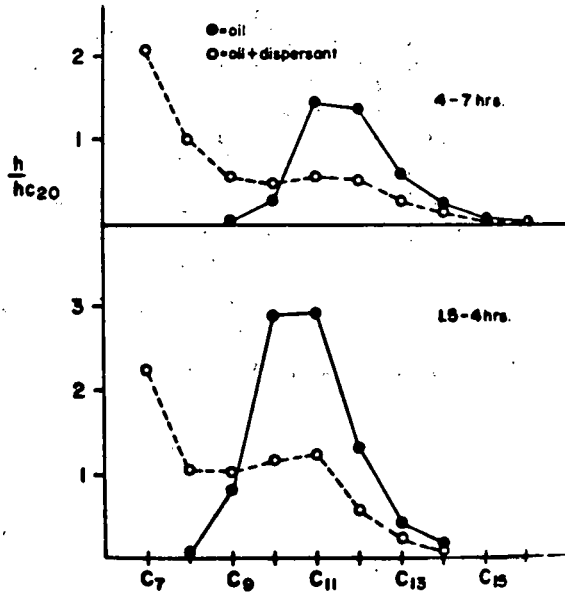


Figure 7.3.3a Evaporation Rates of n-C₇, n-C₈ and n-C₉. Experiment 16.

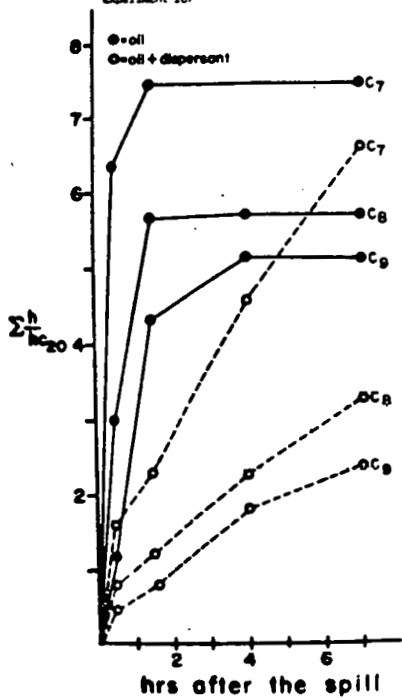


Figure 7.3.3b Evaporation Rates of n-C₁₀, n-C₁₁ and n-C₁₂. Experiment 16.

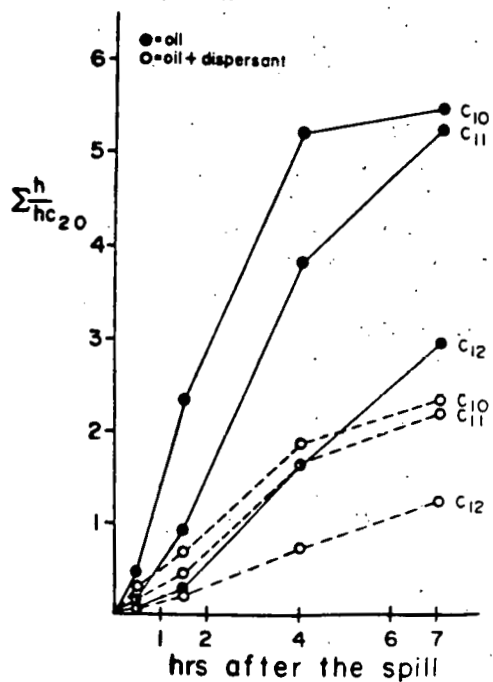
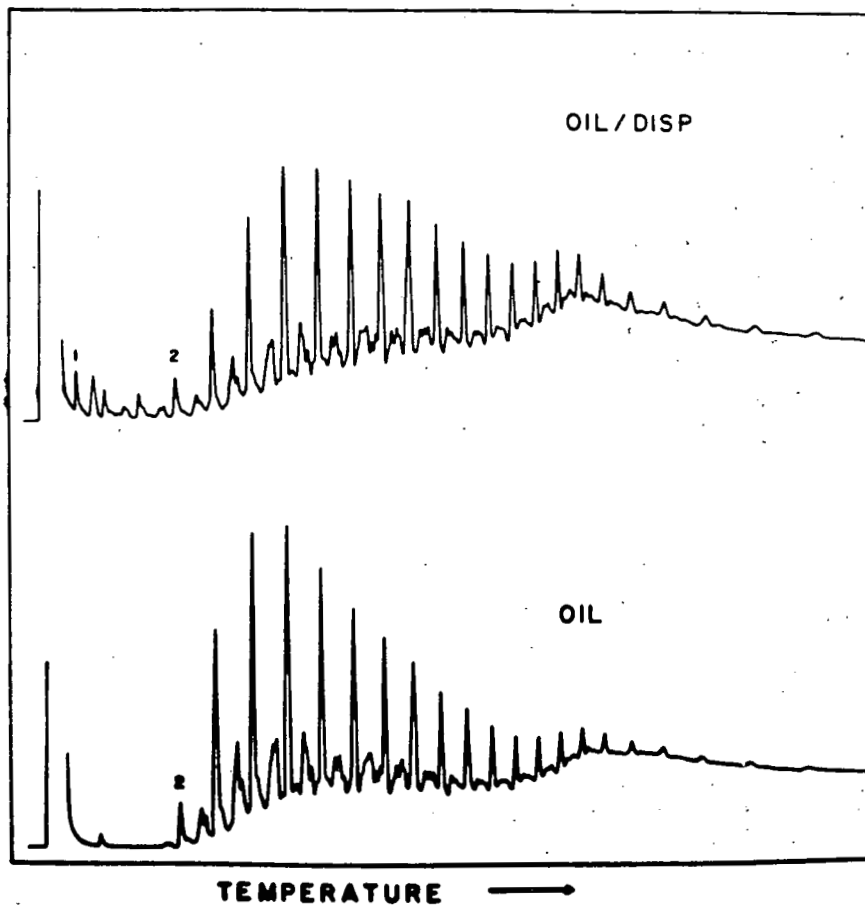


Figure 7.3.36 GC of surface samples taken 7 hours after the oil was added. Exp. 16



evaporation rate. The dispersant affected the evaporation of the lighter n-alkanes to a greater extent than the heavier ones. The slower evaporation of the treated slick could be due to the mixing of some of the oil into the water column. The oil would then be less exposed to the air and it would take longer for the light components to evaporate.

Since the surface areas of the flasks used in the laboratory experiments were limited, the dispersed oil was stopped by the wall of the flasks and some of it accumulated along the walls. Therefore, the oil was not dispersed as efficiently as it would have been if the surface area was infinite. Therefore, the walls may have caused the dispersant to have a different effect on the evaporation in the laboratory experiments compared to that in the open sea, since in the open sea, the dispersion of oil would be greater.

II Long Path Gas Cell

(A) Predicting the Effects of Medium and Low Resolution Infrared Spectrometers

In working in the field, one is often forced to use low-resolution, portable spectrometers. The performance of these instruments is obviously inferior to a high-resolution research-grade laboratory instrument. This work is involved with using a high resolution infrared spectrometer to predict the performance of low resolution instruments. Spectra of single and multi component mixtures of hydrocarbon vapors are used to measure and predict the results of low and high-resolution spectrometers. In this way, the effects of low resolution spectra in quantitative infrared analysis can be measured and predicted. Various spectral manipulation and subtraction techniques are also demonstrated in this work.

This study is done with methane, ethane and propane vapors, individually and in two and three component mixtures. This work was confined to the carbon-hydrogen stretching region, from 3250 to 2790 cm^{-1} . High resolution spectra were taken at a spectral bandwidth of 1.6 cm^{-1} . This is a reasonable value for a laboratory instrument. Lower resolution spectra were observed at bandwidths of 10, 25 and 50 cm^{-1} . High resolution spectra can be convoluted, or mathematically filtered, to reproduce the effects of a lower-resolution spectrum. In this way, a low resolution spectrum can be both measured, as well as predicted from the convolution of a high-resolution spectrum of the same sample.

The equation for a Gaussian slit function is given by:

$$G = \frac{1}{\sigma\sqrt{2\pi}} \exp\left[-\frac{1}{2}\left(\frac{x-\bar{x}}{\sigma}\right)^2\right]$$

$$\text{where width at } \frac{1}{2} \text{ height} \equiv W = 2\Delta\nu_{\frac{1}{2}} = 2\sigma\sqrt{2\ln 2}$$

$$W = 2.354\sigma$$

This is one of the models of spectral slit functions which are currently used in mathematically describing a spectral peak. Convolution is a

process in which a mathematical modification function is imposed on the function of the spectral peak. This process is used in filtering and smoothing spectral data. In this case, a high-resolution spectrum can be convoluted with a Gaussian function to produce a spectrum of lower resolution. One of the purposes of this work is to observe how a mathematically convoluted spectrum compares with a measured spectrum at the same spectral slit width.

Figure 7.3.37 shows a high resolution spectrum of methane vapor, in the 3250-2750 cm^{-1} region. The detail in such a high resolution spectrum makes identification and quantitation of a compound relatively simple. In a spectrum of lower resolution, this detail is lost or reduced, making identification more difficult. This loss of detail also occurs in convoluted spectra. One can compare the results of a low resolution spectrum with a high resolution spectrum convoluted to a lower resolution. This is illustrated in Figure 7.3.38. This shows convoluted and measured spectra of methane vapor from 3250 to 2750 cm^{-1} . The resolution of these spectra was 10, 25 and 50 cm^{-1} , respectively. The sample in all cases is the same, the spectral conditions being modified for each spectrum. Here, one can see the good agreement in the real measured spectra and the predictions made by convoluting the high resolution spectrum.

In convoluting a spectrum, different procedures can be followed. A spectrum can be convoluted to a given resolution in one step, or in a series of "smaller" convolutions. Figure 7.3.39 illustrates this, using a methane spectrum convoluted to 25 cm^{-1} resolution in two different ways. The first spectrum is a convolution of a high resolution spectrum to 25 cm^{-1} in one step, in 0.1 cm^{-1} increments. This refers to the frequency of application of the convolution; here, the function was applied to the data at 0.1 cm^{-1} intervals. The second spectrum shows a different convolution procedure. In the first step, the high resolution spectrum was convoluted to 5 cm^{-1} resolution in 0.1 cm^{-1} increments, and then this spectrum was further convoluted to 25 cm^{-1} resolution in 1 cm^{-1} increments. This two step convolution has the effect of a one-step convolution to 25 cm^{-1} resolution. The difference in the increments applied in the two steps has the effect of smoothing the resultant spectrum when compared to the one step convolution. The variations in the two methods of convolution is significant, suggesting that the convolution procedure used could make a considerable difference in a given circumstance.

Real vapor samples are more frequently mixtures of two or more components rather than a single pure compound. Figure 7.3.40 shows complete spectra of methane, ethane and propane, showing the differences in band structure of the three compounds.

In predicting the appearance of spectra of mixtures, there are a variety of possible approaches. Absorbance spectra of individual pure compounds can be added to produce a synthetic spectrum of a multicomponent mixture of the compounds involved. An important question is how such synthetic spectra compare with convoluted spectra of real multicomponent mixtures.

Figure 7.3.41 shows three spectra of a two component mixture of methane and ethane. Here, the major peaks of each component are approximately equal in absorbance. This shows a high-resolution spectrum, as

Figure 7.3.37 High Resolution Spectrum of Methane Vapor

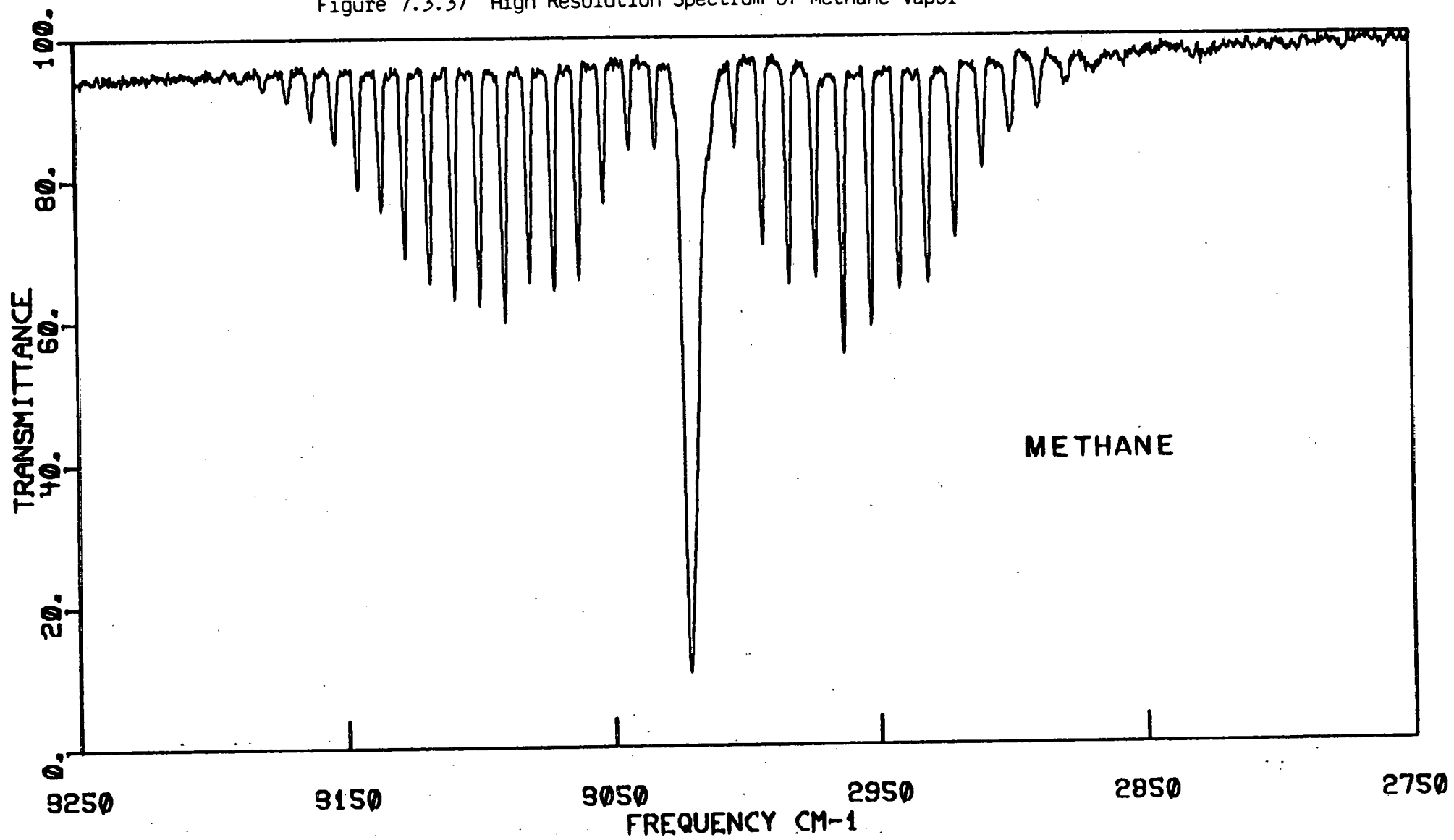


Figure 7.3.38 Convolved and Measured Spectra of Methane Vapor

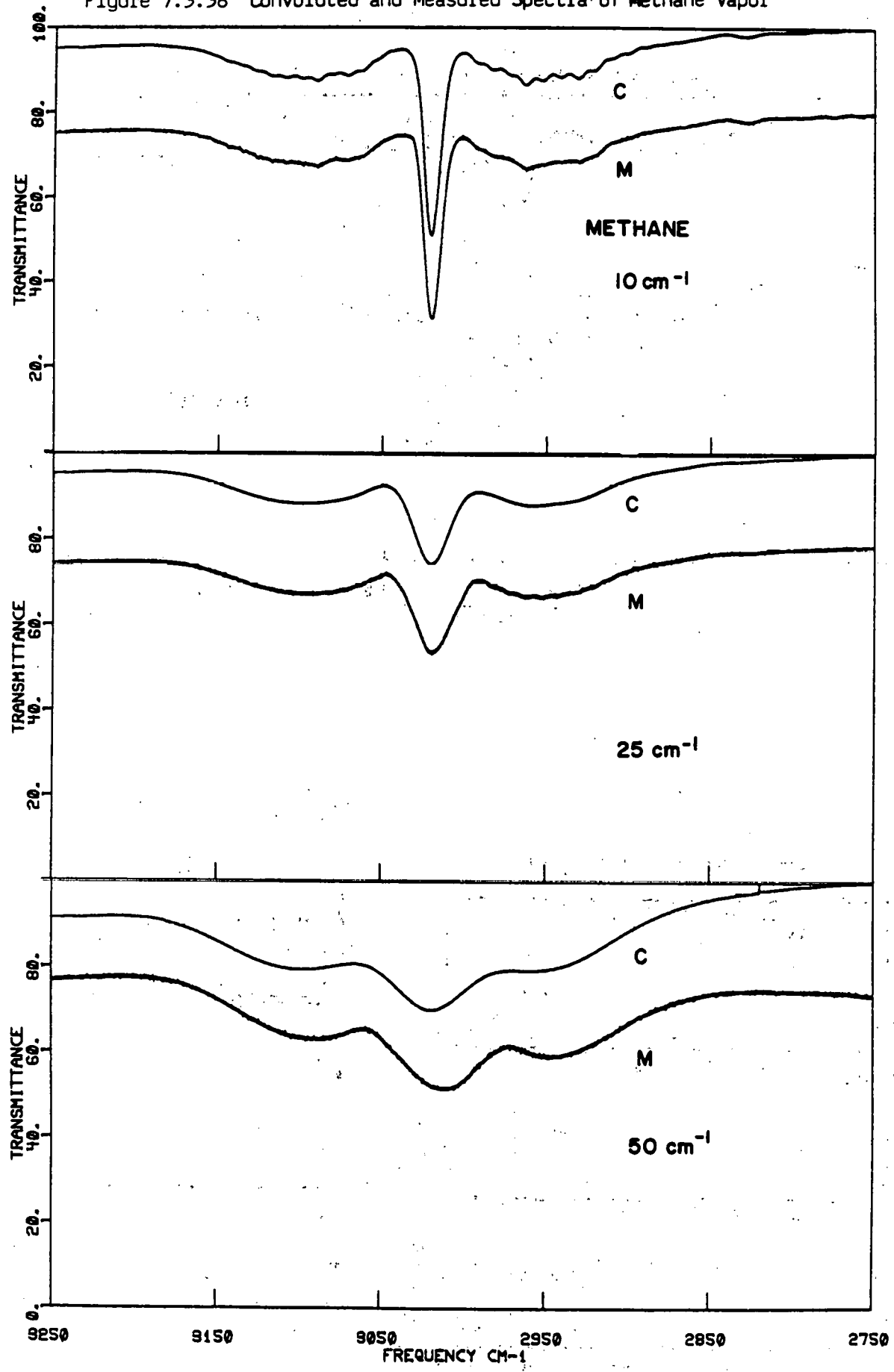


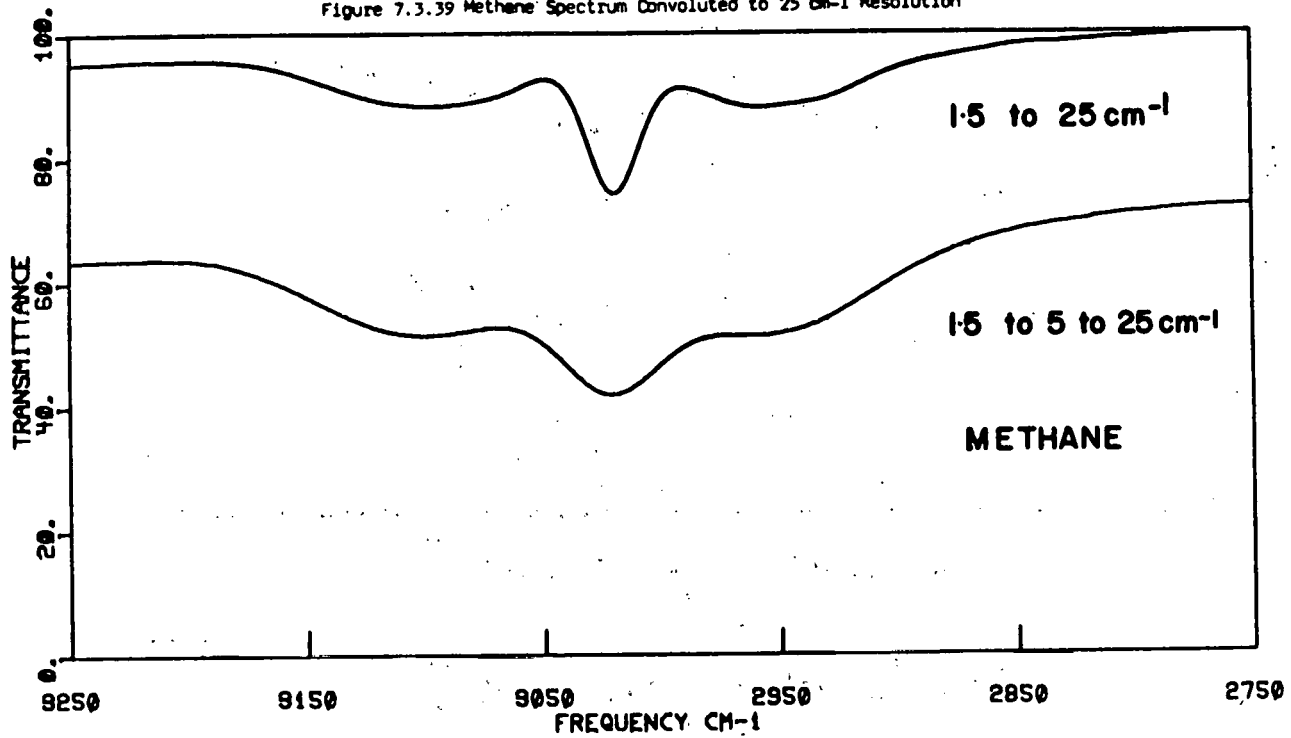
Figure 7.3.39 Methane Spectrum Convolved to 25 cm^{-1} Resolution

Figure 7.3.40 Spectra of Methane, Ethane and Propane

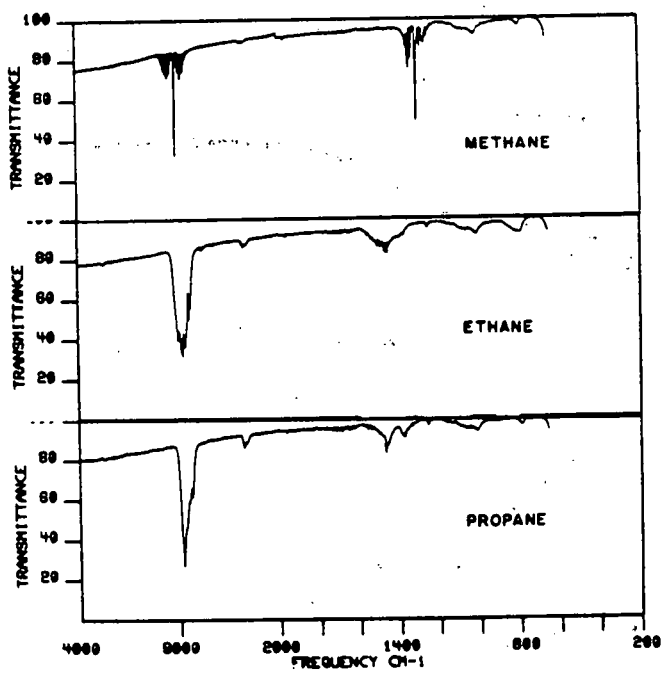
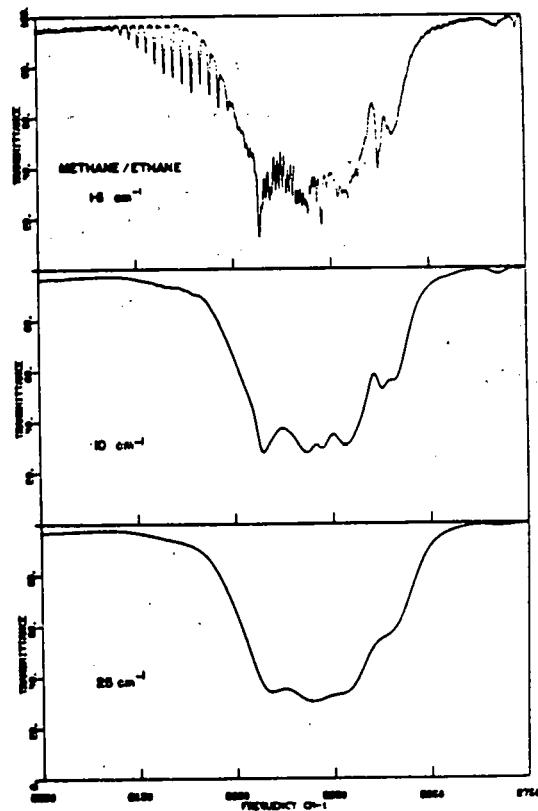


Figure 7.3.41 Two Component Mixture of Methane and Ethane



well as two convolutions, two resolutions of 10 and 25 cm^{-1} , respectively. Once again, most of the spectral information is lost as the resolution decreases.

The following figures illustrate spectral subtraction. The spectrum of a pure compound can be subtracted from the spectrum of a mixture, leaving the spectrum of the remainder of the mixture. In this simple example, the spectrum of ethane is subtracted from the spectrum of the methane/ethane mixture. Theoretically, this should result in the spectrum of methane, the other component of the mixture. Figure 7.3.42 shows the spectra of the methane/ethane mixture, and the pure ethane being subtracted from it. Figure 7.3.43 shows the results of the subtraction, and a real measured spectrum of methane for comparison. One can see that spectral subtraction can be very effective in separating components of a mixture.

The question arises whether this procedure can be used as effectively at lower resolutions. Figures 7.3.44 and 7.3.45 repeat the above experiment, with all spectra convoluted to a resolution of 25 cm^{-1} . One can see that lower resolutions apparently have little effect on the subtraction procedure.

In predicting the appearance of a spectrum of a mixture, spectral addition can be used. The absorbance spectra of the individual components can be added to give a synthetic spectrum of a "mixture" of the components. A comparison of added spectra with a real convoluted mixture is shown in Figure 7.3.46. The first spectrum is a high-resolution spectrum of the methane/ethane mixture convoluted to a resolution of 25 cm^{-1} . The second spectrum illustrates how two spectra can be added and then convoluted. Here, the high-resolution spectra of methane and ethane are added, and the resultant sum is convoluted to 25 cm^{-1} . The third spectrum shows the procedure of convolution, then addition. Here, the two high resolution spectra are individually convoluted, and then added together. These three spectra illustrate the prediction of performance of a low resolution instrument using a high-resolution instrument and computer. A low resolution spectrum of a mixture can be predicted from high resolution spectra of each of the components of the mixture. This can be done either by addition and then convolution to the desired resolution, or vice versa.

The following work with ethane and propane reproduces the results just shown with methane and ethane. Figure 7.3.47 gives a high resolution spectrum of a one to one absorbance mixture of ethane and propane, from 3250 to 2790 cm^{-1} . This spectrum is also shown convoluted to resolutions of 10 and 25 cm^{-1} . Figure 7.3.48 and 7.3.49 show the subtraction of propane from the mixture of propane/ethane, giving a spectrum of ethane. These are all high resolution spectra. Figures 7.3.50 and 7.3.51 duplicate this subtraction for spectra convoluted to a resolution of 25 cm^{-1} .

The results shown above can be extended to mixtures of more than two components. Figures 7.3.52 show spectra of a mixture of methane, ethane and propane in the 3250 to 2750 cm^{-1} region. The two spectra are a high resolution spectra, and the convolution of this spectrum to a resolution of 25 cm^{-1} . Subtractions can be made in a three component system to sequentially extract each component from the system. Figure 7.3.53 shows

Figure 7.3.42 Spectra of Methane/Ethane Mixture and Pure Ethane Being Subtracted From It.

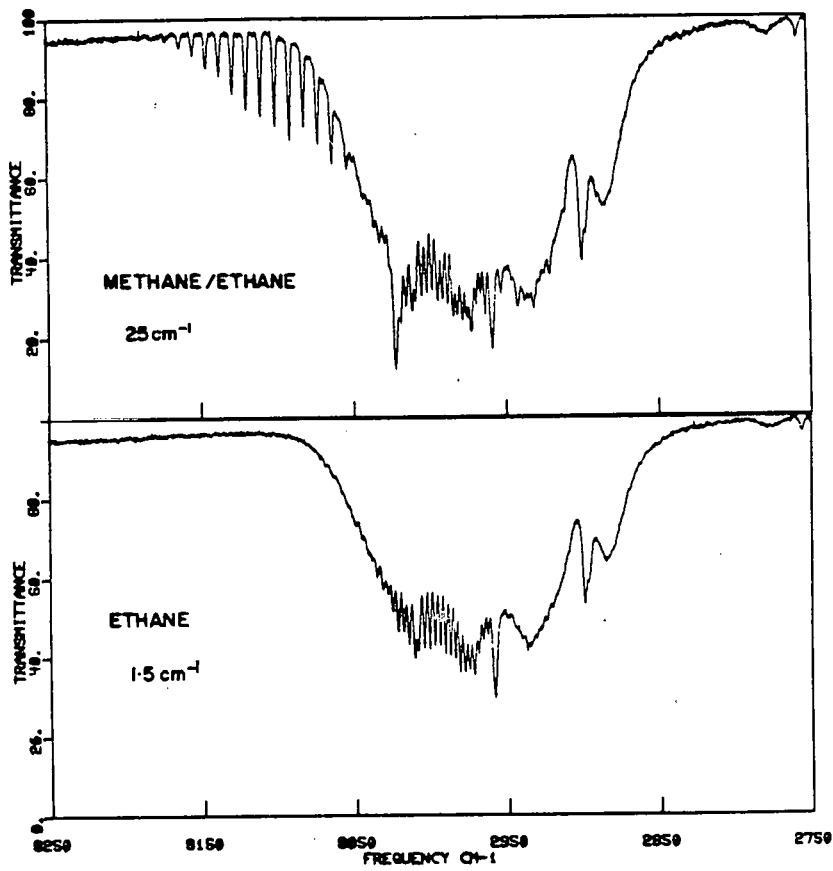


Figure 7.3.43 Results of the Subtraction and a Real Measured Spectrum of Methane

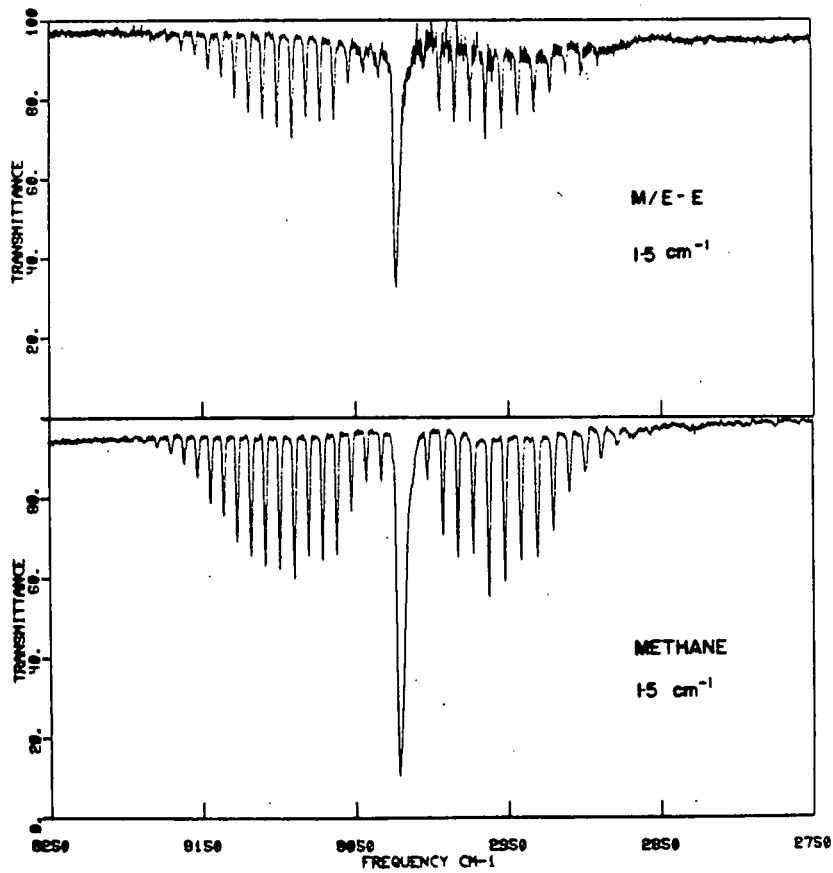


Figure 7.3.44 Spectra of a Methane/Ethane Mixture and Ethane that have been Convolved to 25 cm⁻¹

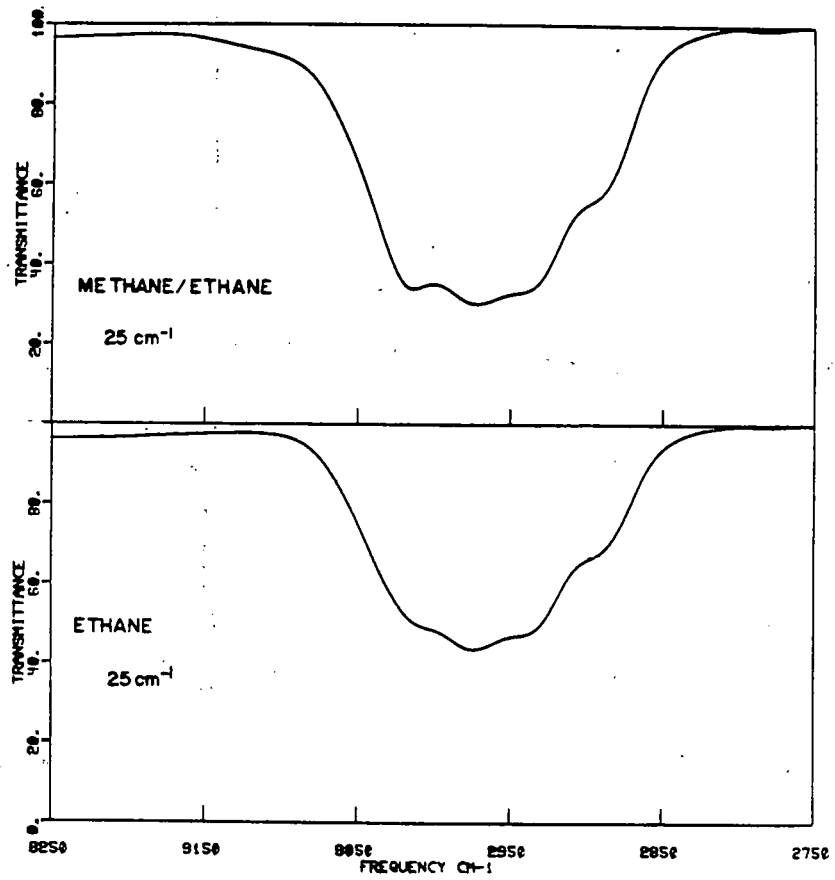


Figure 7.3.45 Convolved Ethane Spectrum Subtracted from Convolved Spectrum of pure methane (bottom)

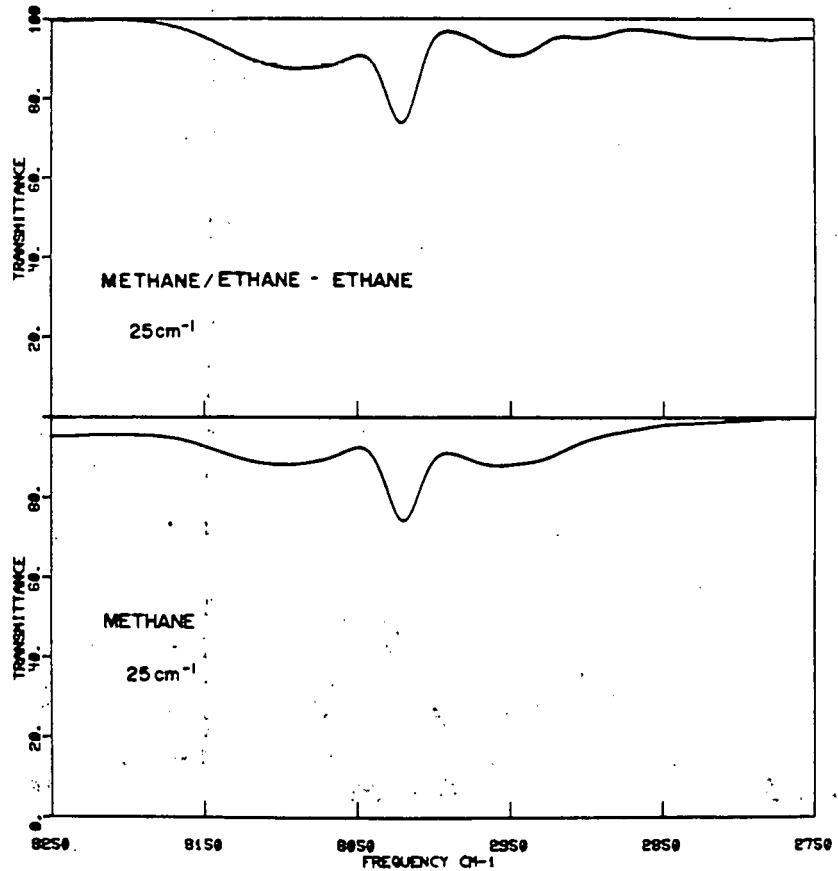


Figure 7.3.46 Results of Computer Addition of Two Spectra Before or After Convolution of Spectra

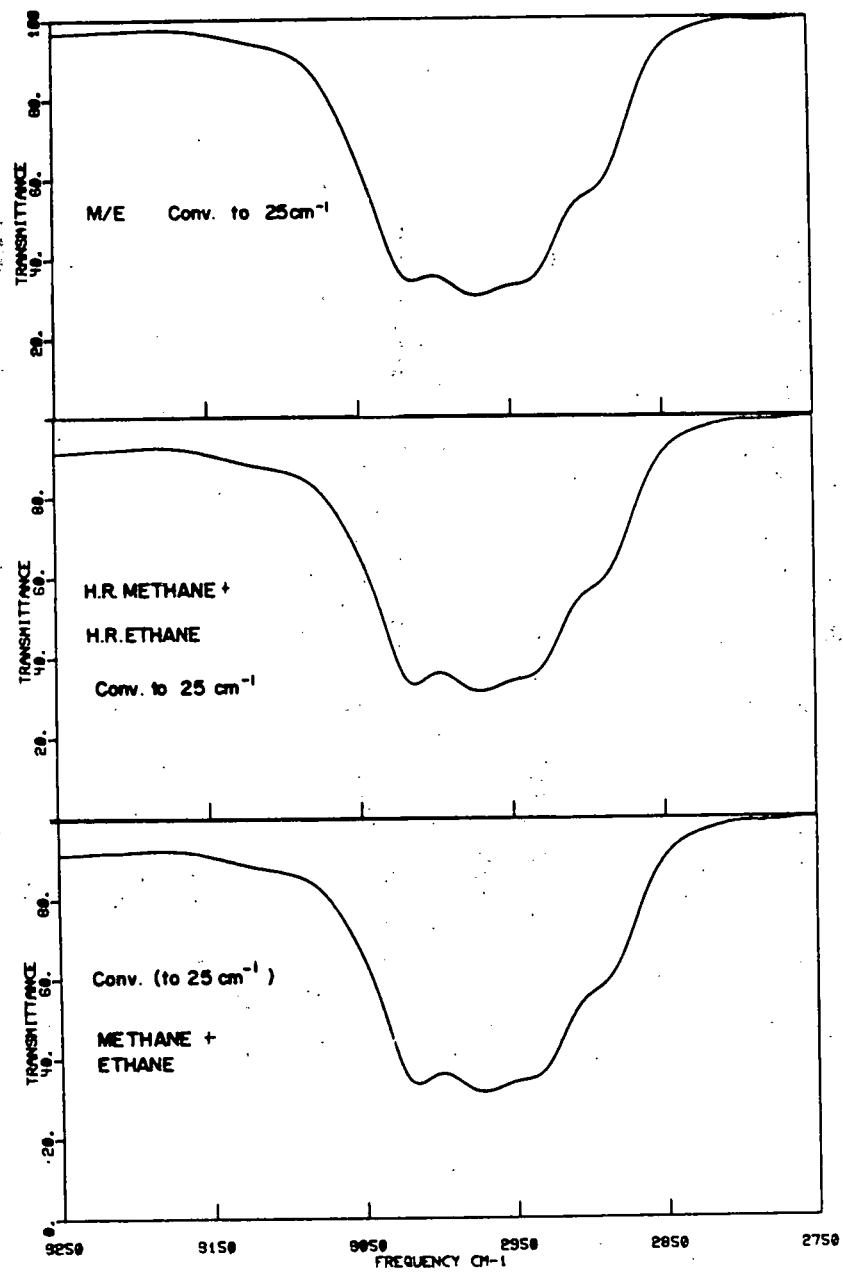


Figure 7.3.47 A High Resolution Spectrum of a One to One Absorbance Mixture of Ethane and Propane

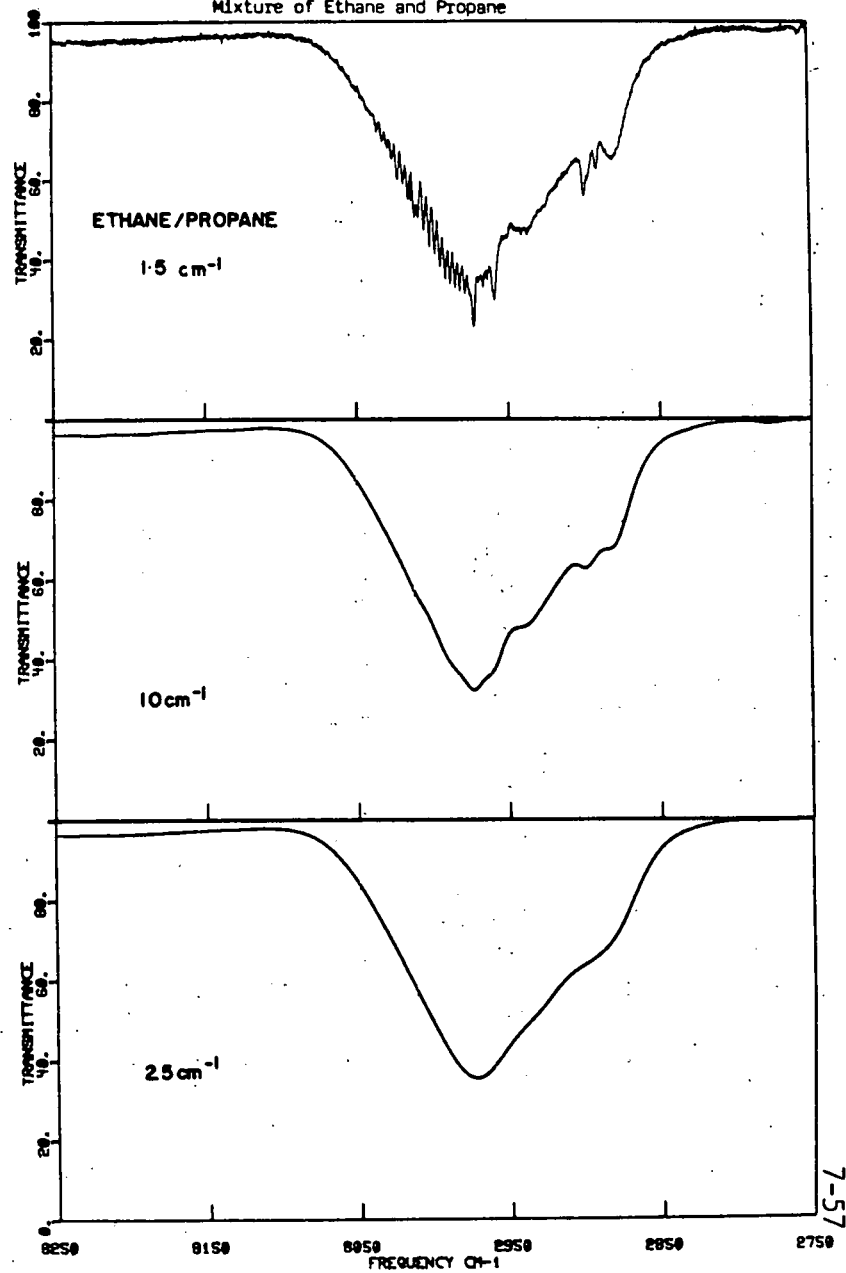


Figure 7.3.48 Subtraction of Propane from the Mixture of Propane/Ethane

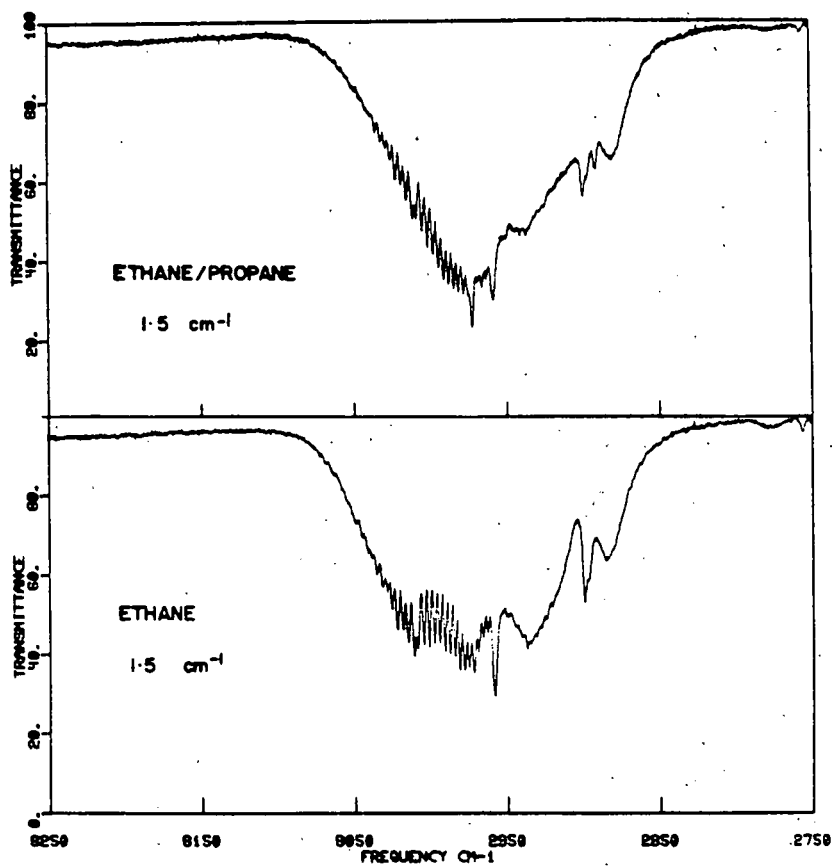


Figure 7.3.49 Subtraction of Propane from the Mixture of Propane/Ethane

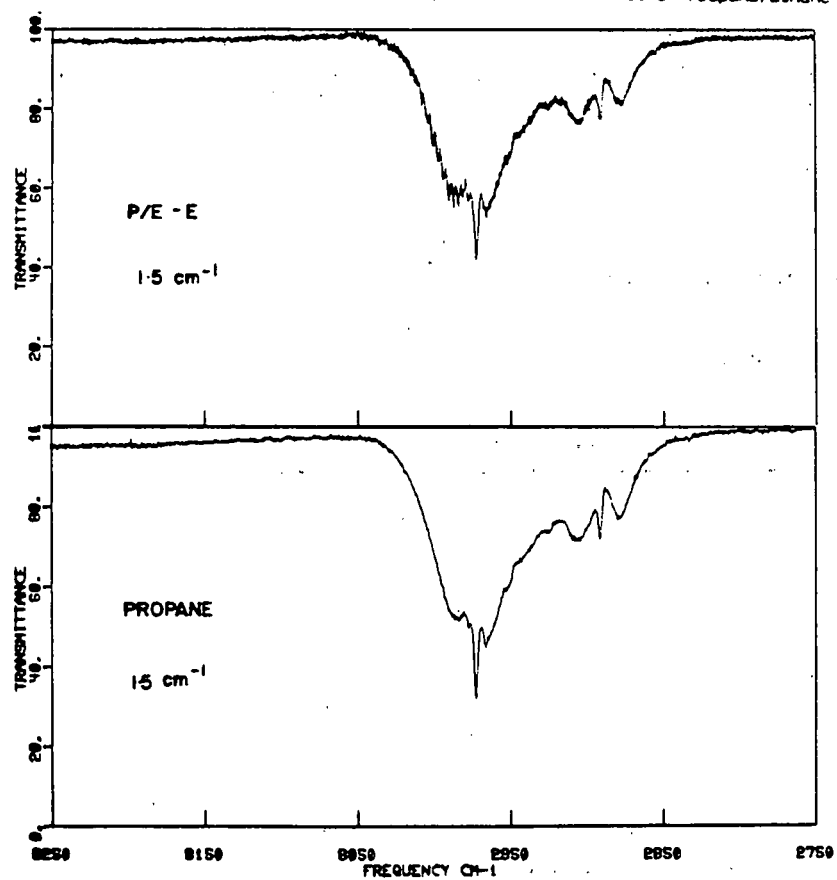


Figure 7.3.50 Convolted Spectra of Ethane/Propane Mixture and of Pure Ethane

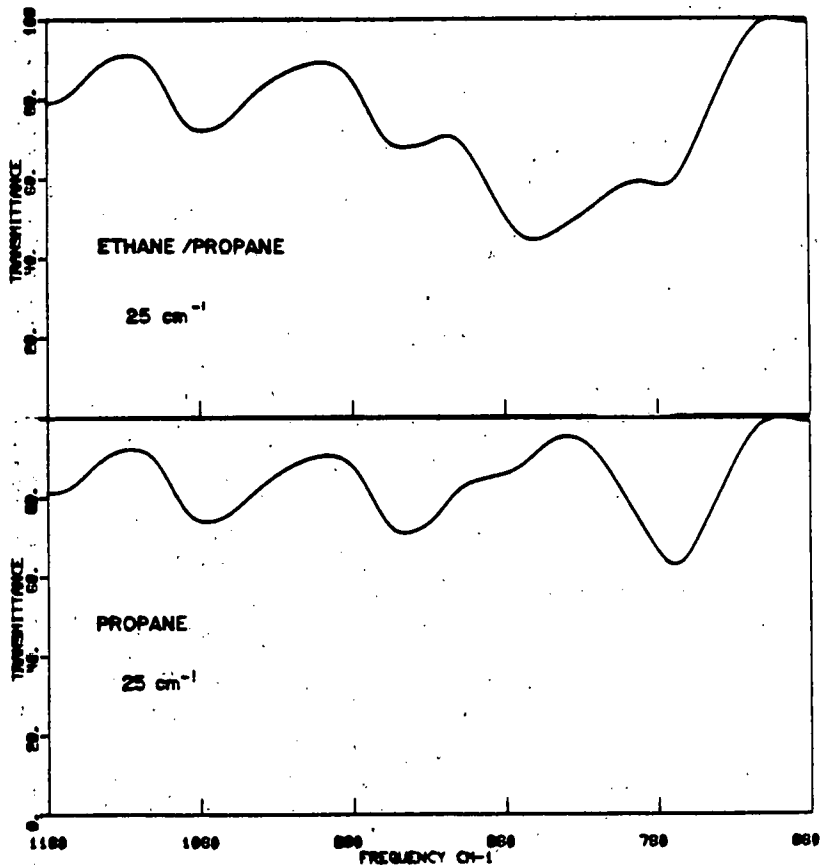


Figure 7.3.51 Subtraction of Convolted Propane Spectrum from Convolted Ethane/Propane Spectrum (top) and Convolted Spectrum of Pure Ethane

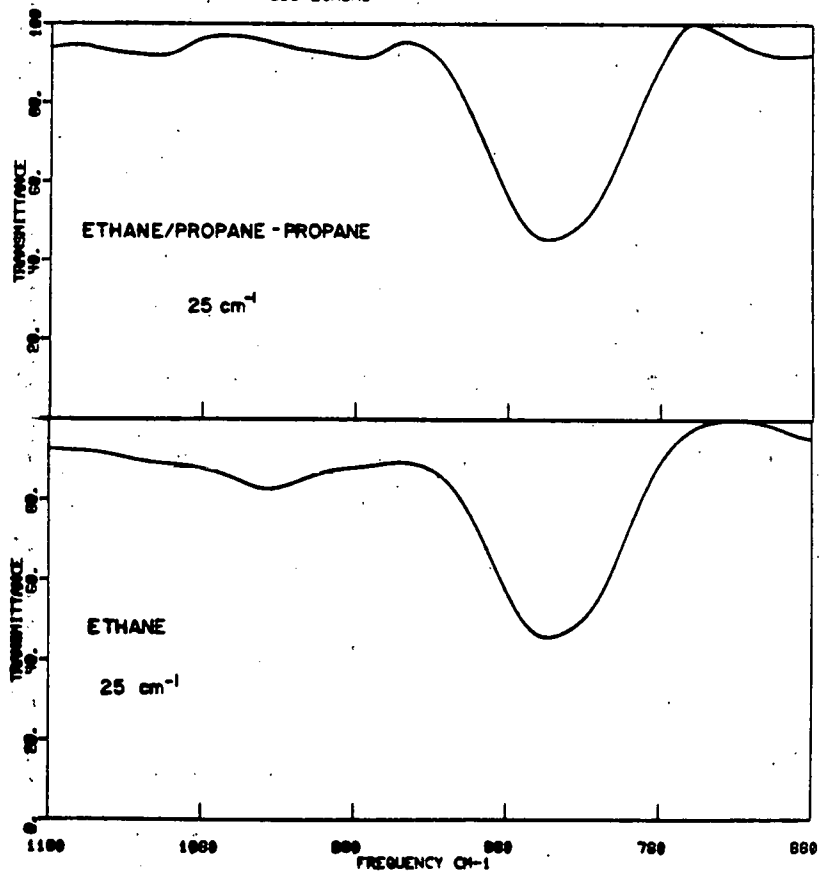


Figure 7.3.52 Spectra of a Mixture of Methane, Ethane and Propane

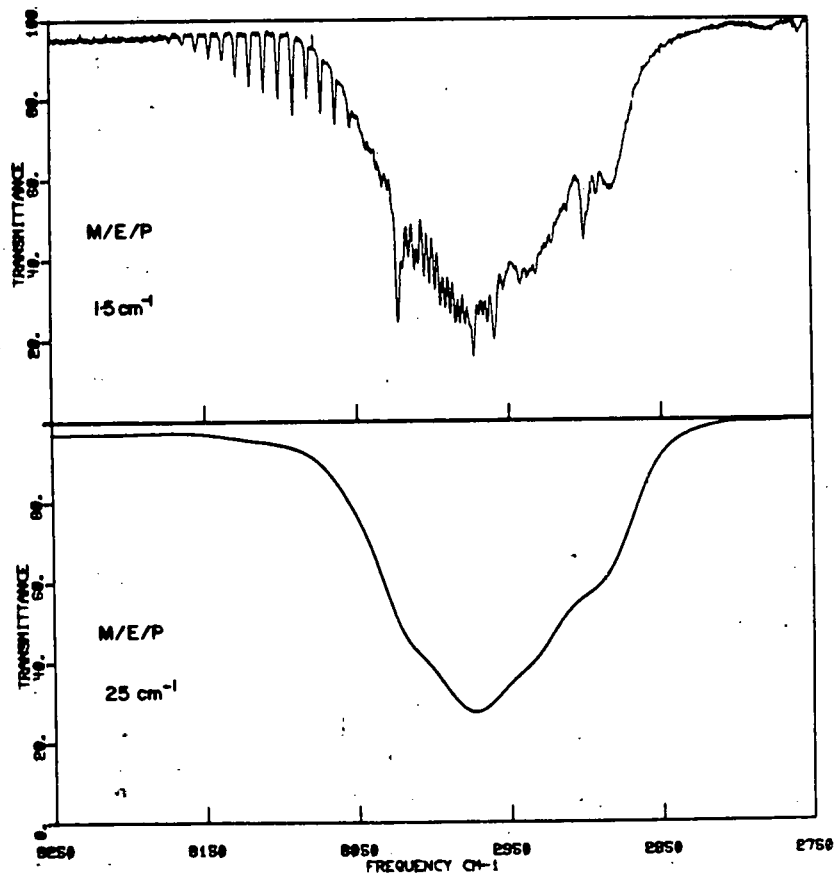
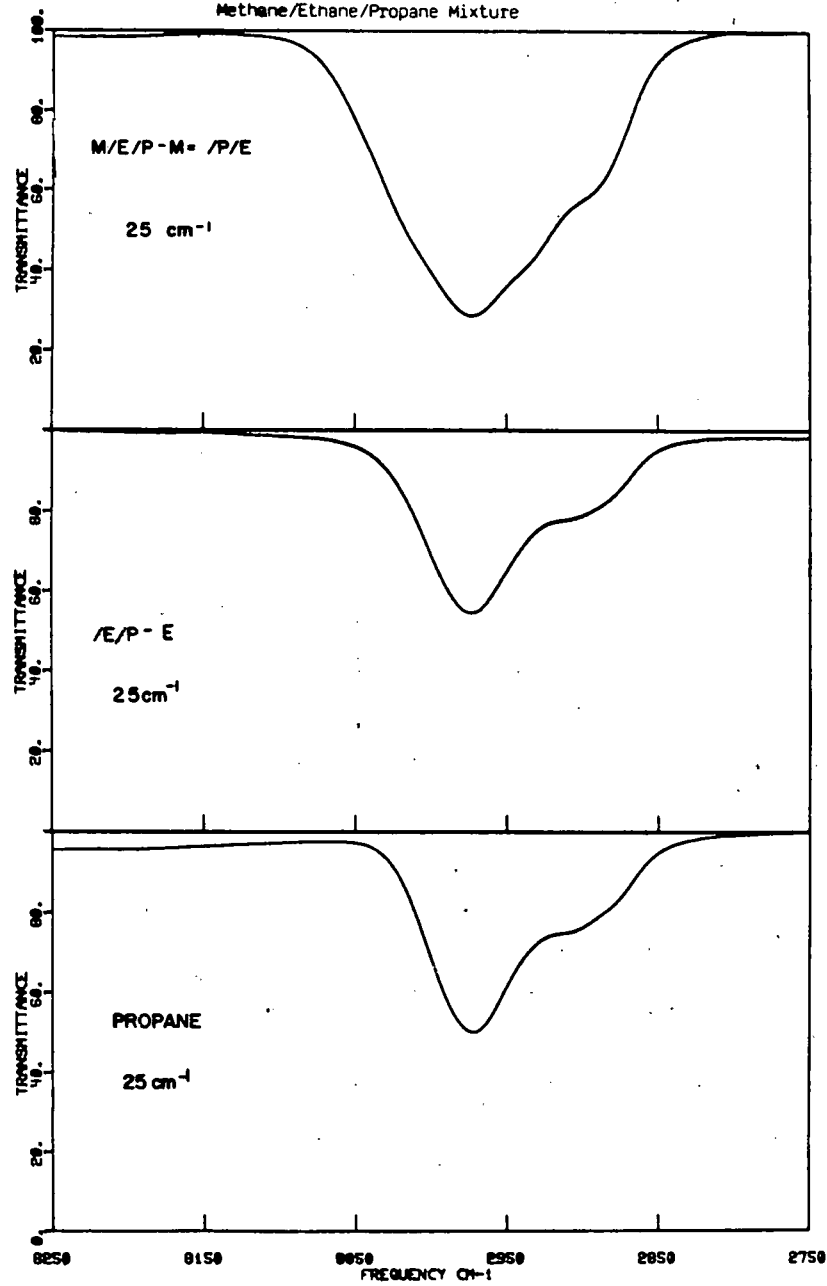


Figure 7.3.53 Sequential Subtraction of Convolved Spectra of methane (1) and Ethane (2) from the Convolved Spectrum of a Methane/Ethane/Propane Mixture



this type of subtraction. The first spectrum is the convoluted spectrum of pure methane, subtracted from the convoluted spectrum of the three-component mixture. The second spectrum shows the subtraction of ethane from this first subtraction.

From these two subtractions, one should expect to be left with a convoluted spectrum of propane, the third component of the system. The final spectrum shows the spectrum of propane for comparison. Obviously, convoluted spectra can also be subtracted with reasonable accuracy in spectra of more than two components.

This study illustrates some of the techniques which can be used in manipulating spectra. High resolution spectra can be convoluted to reasonably simulate the performance of low resolution instruments. Thus, the results of such instruments, as in field work, can be predicted to a fair degree. Additions or subtractions to produce a synthetic spectrum can be performed either before or after convolution, and the appearance of this lower resolution synthetic spectrum will be faithful to that produced by a low resolution instrument under the expected conditions. In addition, these techniques do not appear limited to two-component mixtures. Three component systems can be investigated, and one would reasonably expect to be able to work with larger systems as well. Thus, the performance of low-resolution field grade instruments can be predicted from spectra taken in the laboratory. Predictions made in this way may prove valuable in estimating the practicality of a projected study, or the effectiveness of an analysis before the study is begun.

B) Atmospheric Interferences in the Ambient Vapor Sampling System

In ambient air samples, two major interferences prevent the use of IR analysis for hydrocarbons: water and carbon dioxide (CO_2). Water has very strong absorptions in the IR, centered at about 3750 cm^{-1} and 1600 cm^{-1} . CO_2 has two major bands, at 2350 and 675 cm^{-1} . Taken together, these interferences can ruin quantitative results in an ambient sample. The problem is to reduce or eliminate these interferences, without significantly reducing the sensitivity of the system to hydrocarbons. This was tested by introducing toluene (C_7H_8) vapor into the system under various experimental conditions. The spectra which follow illustrate the results.

Spectrum in Figure 7.3.54 is an illustrative spectrum of toluene vapor in nitrogen gas. For this highly concentrated sample, 50 l of liquid toluene were injected and allowed to evaporate inside the flowing system, which was filled with dry nitrogen. This shows the strong absorptions of this hydrocarbon, especially around 3000 cm^{-1} , 1600 cm^{-1} , 1500 cm^{-1} , 1050 cm^{-1} and 700 cm^{-1} .

Spectrum 7.3.55 is a more realistic concentration, in that it was measured by pumping dry nitrogen over the surface of liquid toluene. This is approximately the concentration one would observe with a sampling device directly over a spill of toluene on water. It still shows the bands mentioned above, but greatly reduced in intensity. One can now also see weak bands from CO_2 and H_2O . These are impurities in the nitrogen diluent, or residual impurities in the cell. This and all subsequent spectra were taken at a path length of 21.75 m.

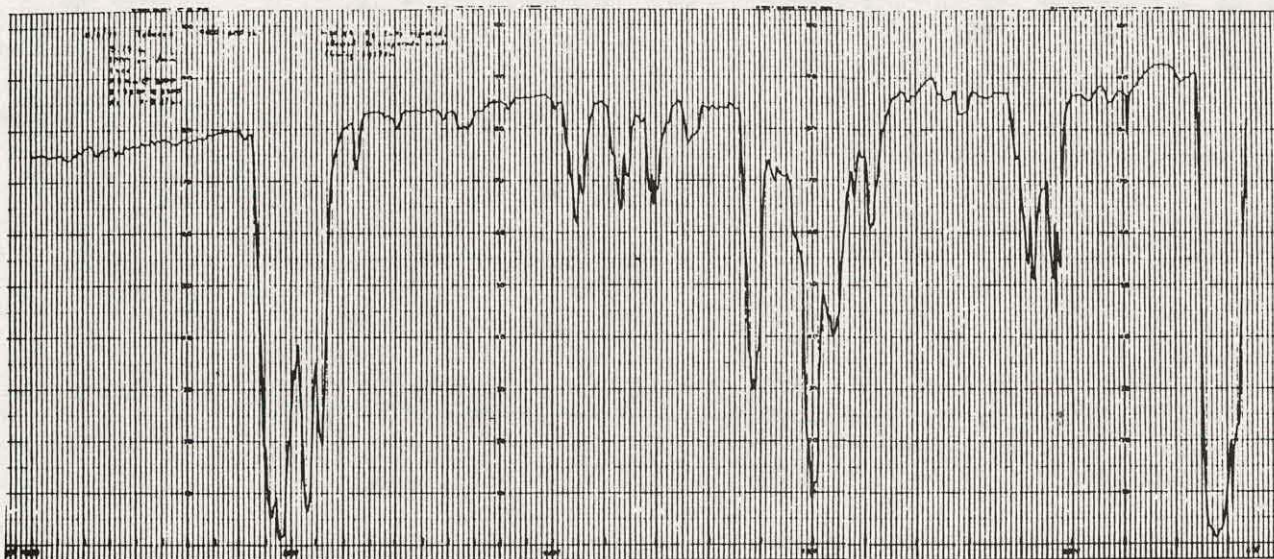


Figure 7.3.54 Illustrative Spectrum of Toluene Vapor in Nitrogen Gas

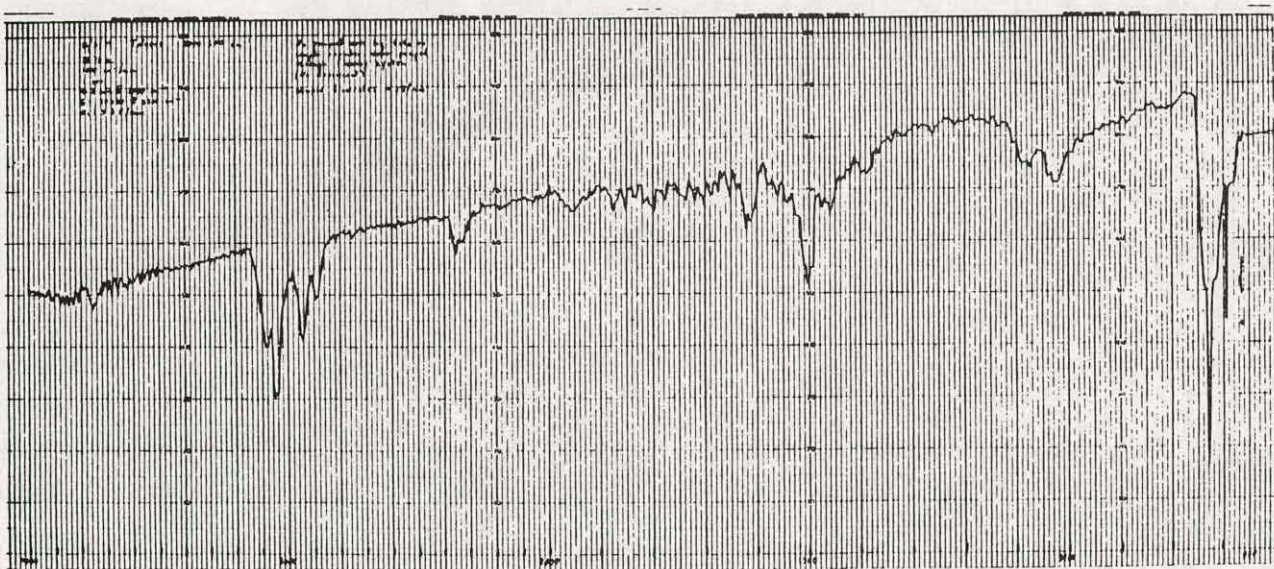


Figure 7.3.55 Spectrum of Toluene Vapor in Nitrogen Gas

Spectrum 7.3.56 is identical to 7.3.55, except for the addition of a drying tube, filled with a calcium sulfate dessicant, (DRIERITE). Most of the peaks are not significantly reduced in intensity, indicating that the Drierite is not removing appreciable amounts of hydrocarbon vapors.

In spectrum 7.3.57, air is used instead of dry nitrogen. Here, all CO₂ bands are clearly seen for the first time. The Drierite will not remove this vapor, although in this case, it is not critical. The toluene can still be easily quantitated by using the bands in the 3000 cm⁻¹ region. Water is still absent, indicating that the Drierite is effectively removing the interfering water vapor from the air. Spectrum 7.3.58 is not critical to the test, but is interesting. Here, a liquid nitrogen cold trap was added to the drying tube. Not only was all water removed, but most of the hydrocarbons were frozen out as well. The small peak at 3000 cm⁻¹ is methane. Whether this is an impurity from the liquid toluene or the air is not known.

Spectrum 7.3.59 shows the spectrum of ambient air and toluene vapor, without any dessicant or filter. This shows the massive interferences present in untreated air, and the extent to which the Drierite is effective. Compare this with spectrum 7.3.57. For all of the above spectra, the flow rate was about 2 l/min past the toluene liquid. This was estimated to be the optimum flow sampling rate. Two factors are important in determining flow rates in sampling: system response time and dessicant effectiveness. As the flow rate increases through the 5.5 l liter cell, the time required to respond to a change in sample composition is decreased. The shorter the response time, the more accurately the system will reflect the concentrations of a given sample as it changes with time, as in an evaporation process. As the flow through in the dessicant is increased, the effectiveness of the Drierite is reduced, as is shown in spectrum 7.3.60. This spectrum was taken with a sampling flow rate of 5 l/min, but is otherwise identical to the conditions for spectrum 7.3.57. It shows the amount of water interference still present in the cell due to the higher flow rate.

It can be concluded that with a suitable dessicant, one can eliminate substances which interfere with quantitative ambient air analysis in the system.

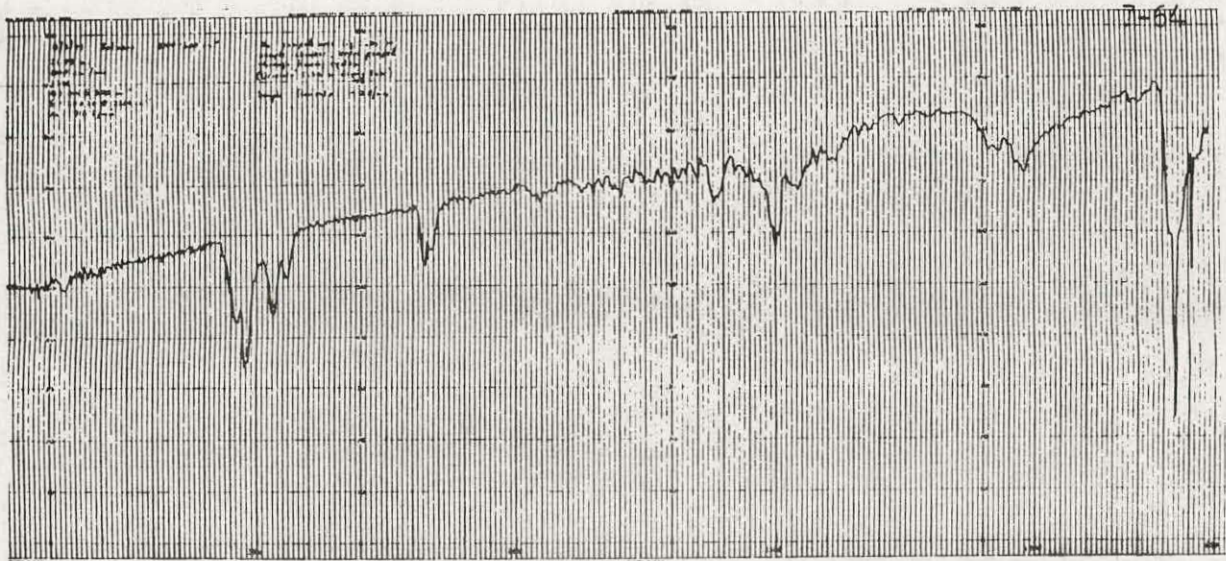


Figure 7.3.56 Spectrum of Toluene Vapor in Nitrogen Gas After Drying Tube was Added to System

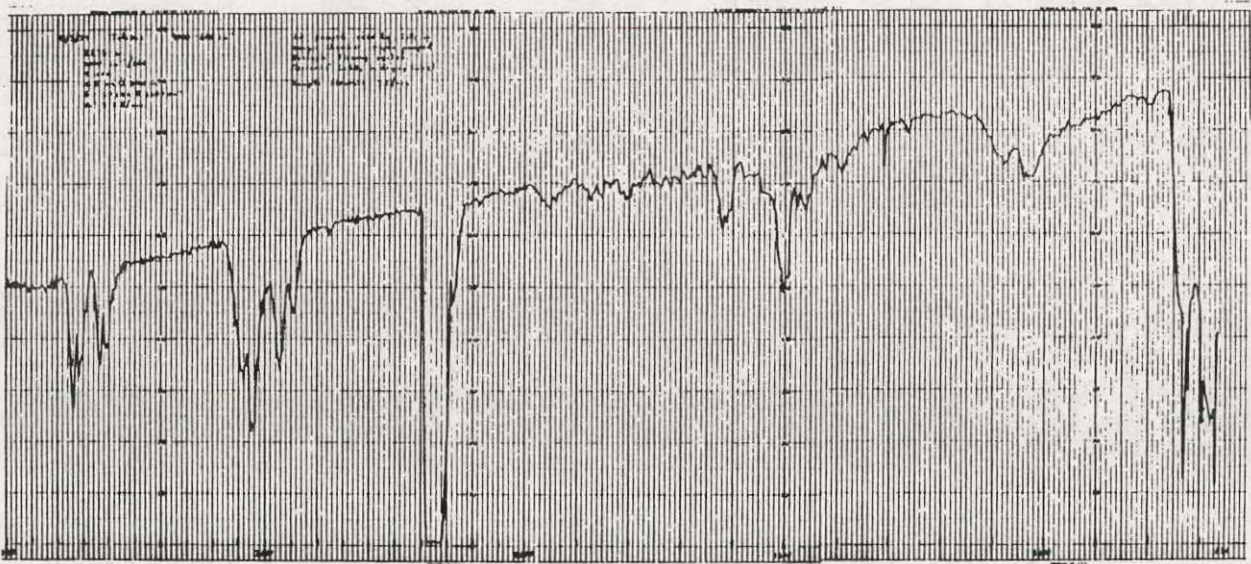


Figure 7.3.57 Spectrum of Toluene Vapor in Air

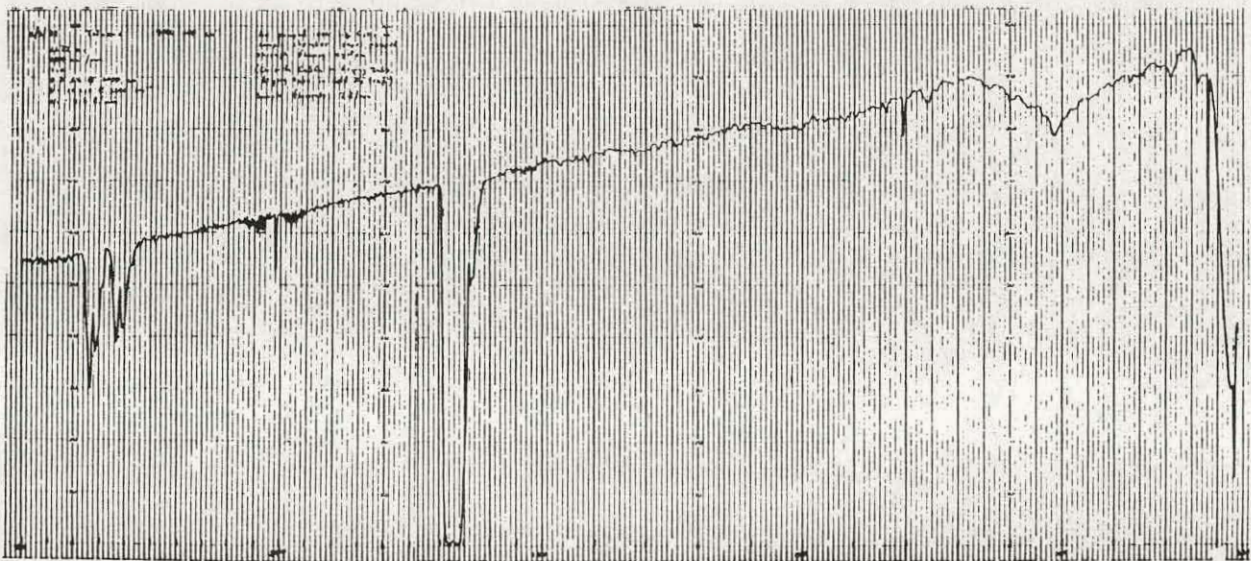


Figure 7.3.58 Spectrum of Air after Cold Trap was Added to System

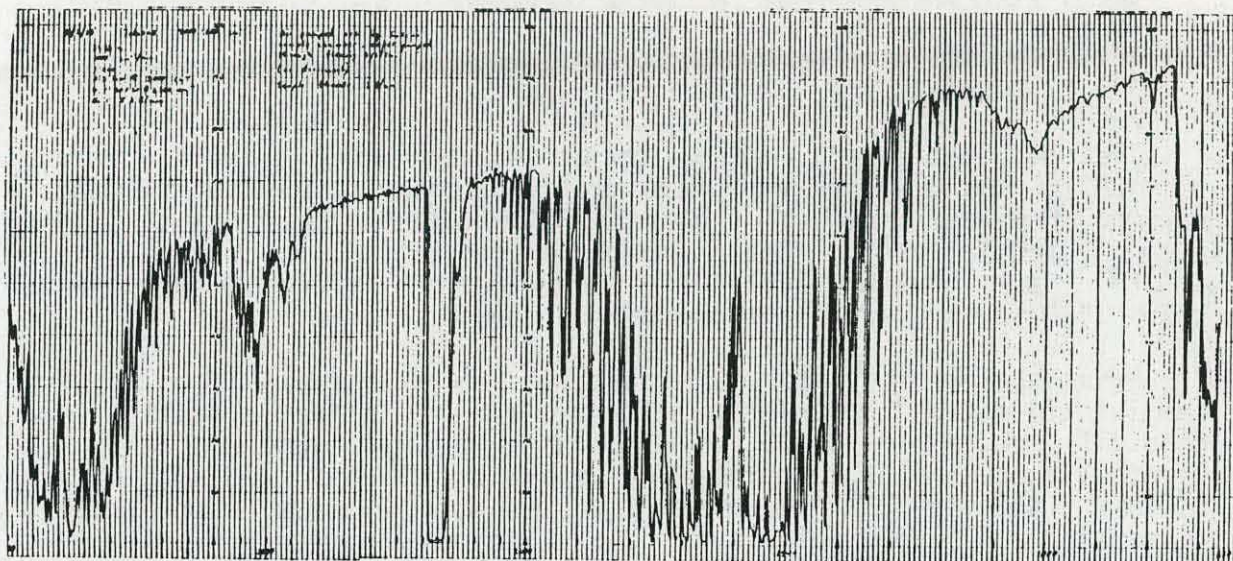


Figure 7.3.59 Spectrum of Ambient Air and Toluene Vapor, without any Desiccant or Filter

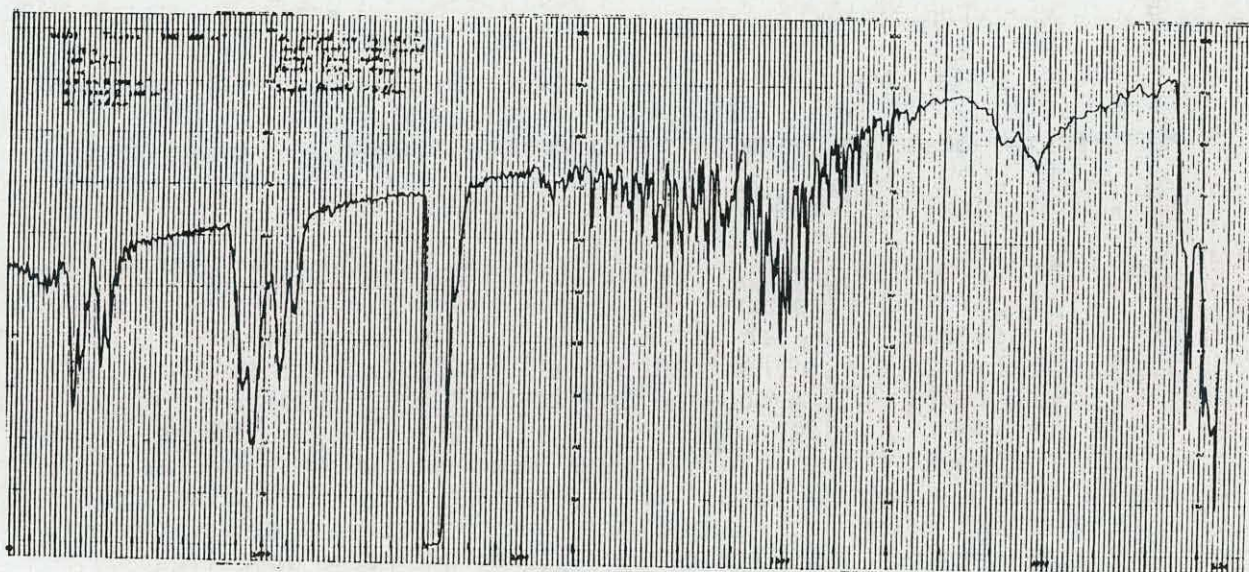


Figure 7.3.60 Spectrum of Ambient Air with Desiccant in System

References

1. M. Ahmadjian, C. Baer, P.F. Lynch & C.W. Brown, Environ. Sci. & Technol., 10, 777 (1976).

7.4 Mesoscale Experiments

7.4.1 Introduction

Treating an oil spill with a chemical dispersant reduces the amount of oil on the surface and increases the concentration in the water column. However, a number of questions need to be answered, e.g., "How much is the increase?" "Does a dispersant affect all components of oil in the same manner?" Is the effect uniform throughout the water column?" How does the effect change with time?"

Presently, we are trying to answer these questions by analyzing water samples collected from beneath both treated and untreated spills. The chemical results are important since they can be correlated with the physical processes of dispersion (1) and with the microbial utilization of the chemicals (2). Furthermore, they will eventually be used to determine the overall effect on the marine environment (3). Herein, chemical analyses of water samples from the meso scale experiments were compared for both treated and untreated spills.

7.4.2 Test Facilities

The meso scale test system, located 450 meters from Narragansett Bay consists of two 4000 liter tanks (6.2 m tall and 0.9 m in diameter). These tanks are described in more detail elsewhere (3).

7.4.3 Chemical Analysis

One liter water samples were extracted with two 15 ml. aliquots of CS_2 . The aliquots were combined and the volume adjusted to 25 ml (some of the CS_2 dissolves in water and some is lost by evaporation to give a total just below 25 ml). The solution was placed in a 6 mm pathlength infrared cell (with AgCl windows), and the infrared absorbance at 2920 cm^{-1} measured with an identical cell containing CS_2 in the reference beam of the spectrometer (4,5). The measured absorbance was then converted to total hydrocarbons from a pre-determined plot of absorbance vs. concentration (separate plots were used for oil and oil/dispersant, and were both obtained using the oil and dispersant being investigated).

The volume of the CS_2 solution was then reduced to .6 ml under nitrogen, and the complete infrared spectrum (IR) was measured under the same conditions as above. Following this, the gas chromatogram (GC) was measured.

IR spectra were measured on a Beckman 4260 spectrometer and GC on a Hewlett Packard 5710A gas chromatograph equipped with flame ionization detection and 10 m x 3 mm column packed with SP2250. The GC temperature was programmed at 8 C/min.

A. Series I

All of these experiments in the meso scale tanks were performed on API Kuwait crude oil, using Corexit 9527 as the dispersant.

Sixty ml of oil (15 ppm total concentration) were added to the water surface in each tank and 12 ml of dispersant to one of the tanks. One liter water samples were collected from each of the three ports at 1, 24, 48 and 72 hours.

In addition, in the first three experiments, 1 liter water samples were collected while the tanks were being filled, and at 30 minutes after filling. These samples were used as controls. In the fourth experiment, a control tank of the same dimension and with the same sampling ports, was used, and samples were taken at the same time as the others.

All water samples were returned immediately to the laboratory for analysis.

Several test runs without oil were made in the meso scale tanks to determine the variation of extractable organics in the tanks. Extracts of water from the tanks were compared with those of water taken directly from Narragansett Bay and, in most cases, the concentration of organics in the tanks and in the Bay were similar. The only major difference was that the tanks were generally higher immediately after filling. This was probably due to the mixing of bottom sediments in the water column.

(a) Water Analysis

Four experiments were performed with oil and oil/dispersant. In all cases, oil was added only to the north tank and oil/dispersant to the south tank. In the experiment using the control tank, it is referred to as the east tank. The weather conditions and other information on the experiments will be discussed separately.

(i) Experiment 1:

Concentrations of extractable organics from the top, middle and bottom ports (1,3,5m) as a function of time are shown in Figures 7.4.1, 7.4.2, and 7.4.3. The control values for the two tanks are given by dashed lines across the plots. Both control values are high. However, the one for the north tank was abnormally high. In this experiment, only one control sample was collected from each tank immediately after filling and, as mentioned above, the abnormally high values are probably due to the suspended sediment.

In the next two experiments, control samples were collected immediately after filling and one half hour later. The latter values are closer to the actual values of organics in sea water.

Considering the high control values, it is difficult to analyze the results of this experiment. However, general trends can be identified. Only one sample from the south tank had a concentration above the control, and that was the top sample collected after 72 hours.

The tank with the dispersant had an extremely high value for the 1 hour sample from the top, but the concentration decreased significantly after 24 hours and continued to decrease for the duration of the experiment. The highest concentration for the middle and bottom ports were found at 24 hours, and these also decreased with time.

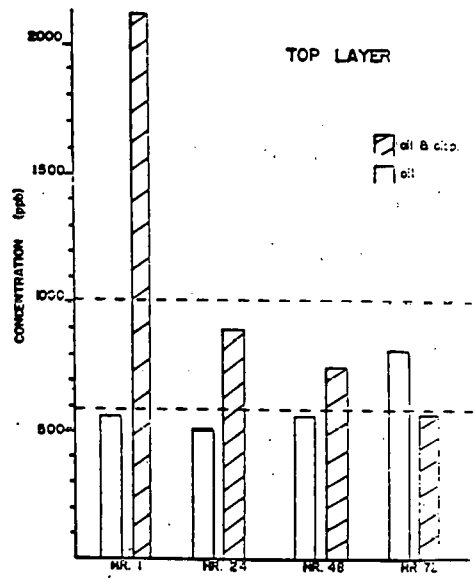


Figure 7.4.1 Concentrations of Extractable Organics from the Top Port (1a) as a Function of Time. (Exp. 1)

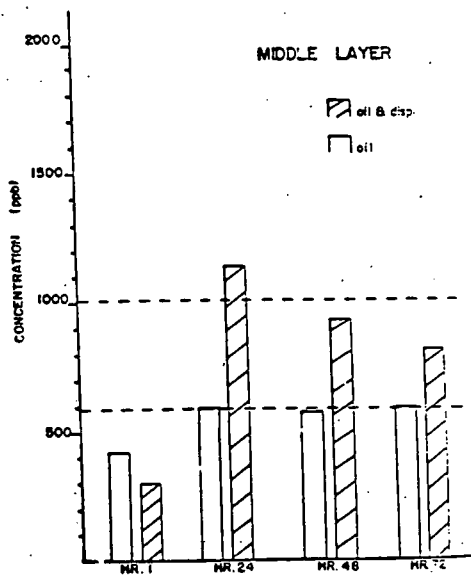


Figure 7.4.2 Concentration of Extractable Organics from the Middle Port (2a) as a Function of Time. (Exp. 1)

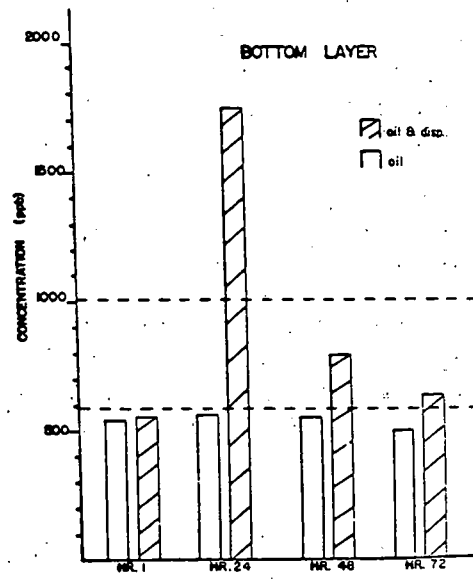


Figure 7.4.3 Concentration of Extractable Organics from the Bottom Port (3a) as a Function of Time. (Exp. 1)

In general, this experiment indicated that dispersant caused a high concentration at the 1 m depth after 1 hour. Some of these chemicals moved toward the surface and others to the bottom during the next 24 hours.

(ii) Experiment 2:

Quantitative values for the total extractable organics from the second experiment in the meso scale tanks are shown in Figures (7.4.4) and (7.4.5). Control values of 210 and 243 ppb are shown as dashed lines drawn horizontally across the bar graph. The time dependence of concentration from the top, middle and bottom sampling ports (1,3, 5.5m) are given in Figure (7.4.5).

In the top port, the concentration of extractable organics (above the concentration of the control) at 1 hour was more than 27 times greater than when the dispersant was used, i.e., 4880 ppb as compared to 180 ppb. After twenty-four hours, the concentration in the tank without dispersant fell to below control level and stayed for the remainder of the experiment. In the treated tank, the concentration of extractable organics decreased by more than a factor of 3 to 1350 ppb after 24 hours, and then gradually decreased to 851 ppb after 3 days.

At the middle level, the concentration in the untreated tank gradually decreased from 324 ppb during the 72 hour experiment, whereas there was a three-fold increase in the tank with dispersant from 1 to 24 hours. This level decreased gradually after twenty-four hours.

The concentration in the bottom layer in the untreated tank reached a maximum slightly above the control level at 24 hours and then gradually decreased. In the tank with dispersant, there was a five-fold increase from 1 to 24 hours, but the maximum was not reached until 48 hours.

For comparison, the same results are plotted in Figure 7.4.5 as a function of depth for each of the sampling times. These plots clearly show that the maximum concentration moved toward the bottom in both the treated and untreated cases. However, there was a significantly greater concentration in the treated tank.

For qualitative comparison of the water sample, two sets of GC are shown in Figures 7.4.6 and 7.4.7. The 24 hour samples are compared in Figure 7.4.6. The GC of the untreated samples was expanded seven times. The distribution of n-paraffins in this sample is not similar to the treated oil and is not characteristic of petroleum. The GC of the top 1 hour treated sample is shown in Figure 7.4.7, where it is compared to all 24 hour samples from the same tank. Components boiling below n-C₁₅, which were initially dispersed, were not found at 24 hours.

(iii) Experiment 3:

The concentration for the top, middle and bottom layer as a function of time are shown in Figures 7.4.8, 7.4.9 and 7.4.10. The initial values for the top are similar to those in experiment 2. However, the decrease in the treated tank after 24 hours was much greater.

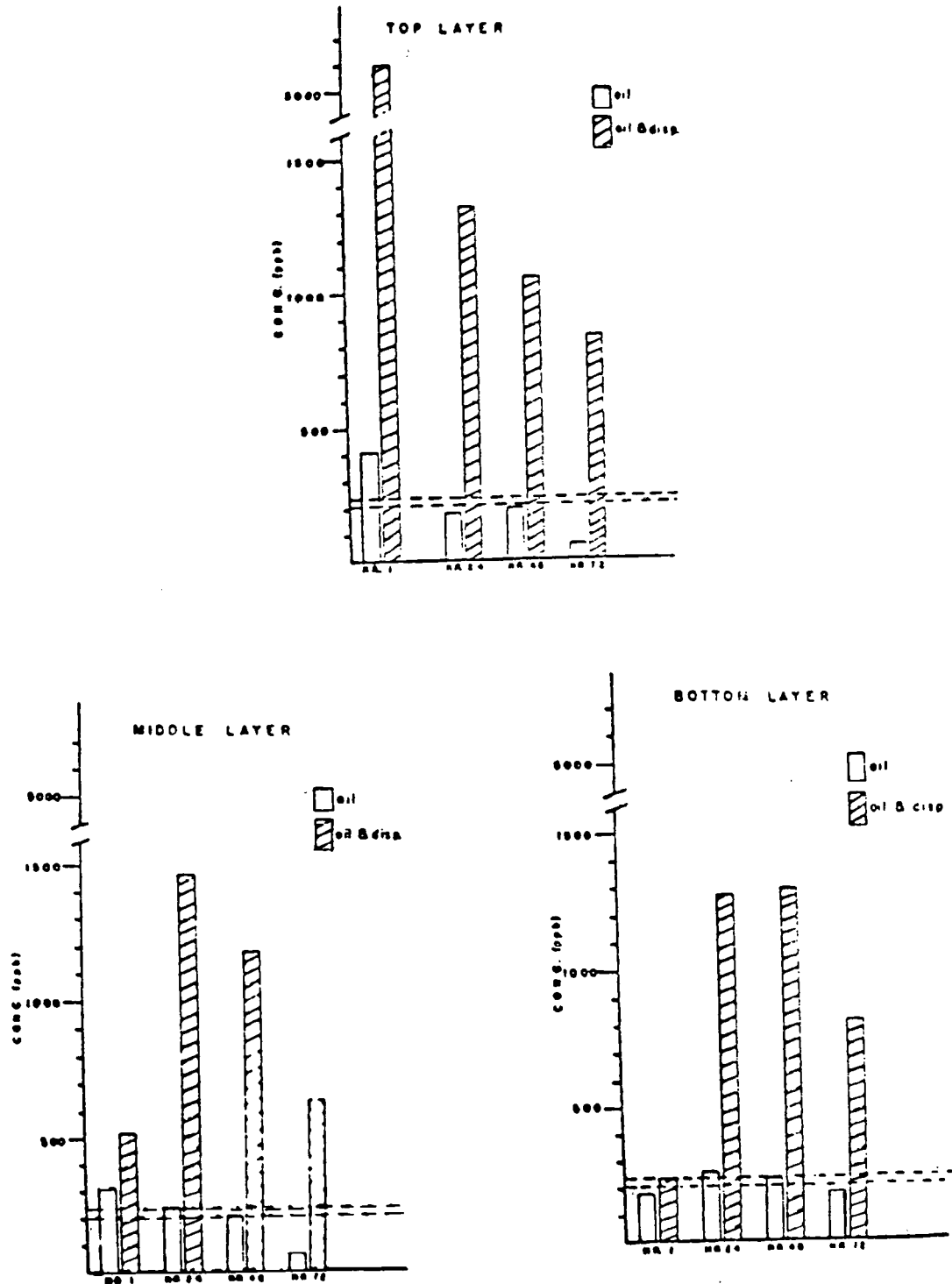


Figure 7.4.4 Concentration of Extractable Organics in the Top, Middle, and Bottom Levels. (Exp. 2)

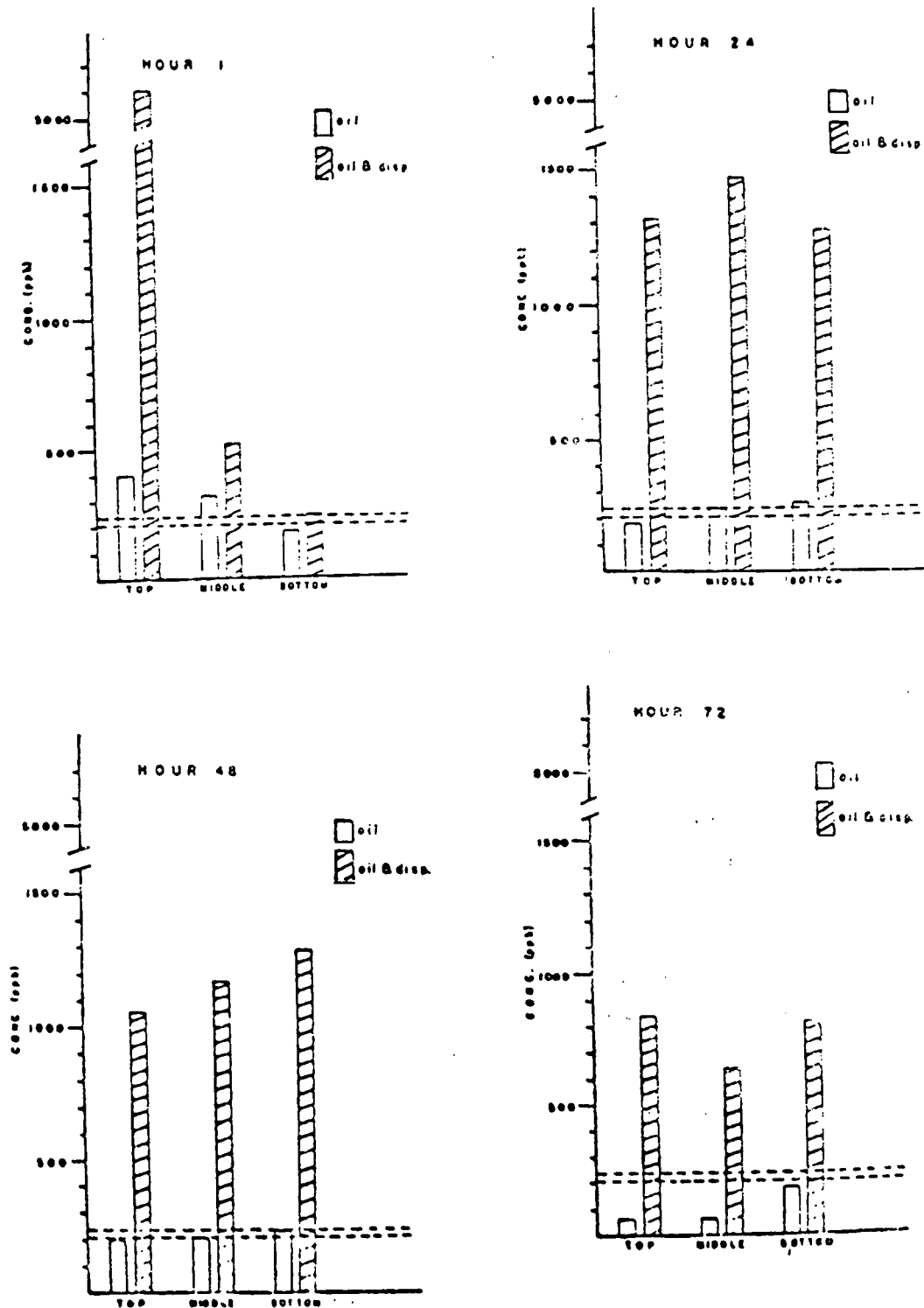


Figure 7.4.5 Concentration of Extractable Organics in the Top, Middle, and Bottom of the Treated and Untreated Tanks at Each Sampling Time

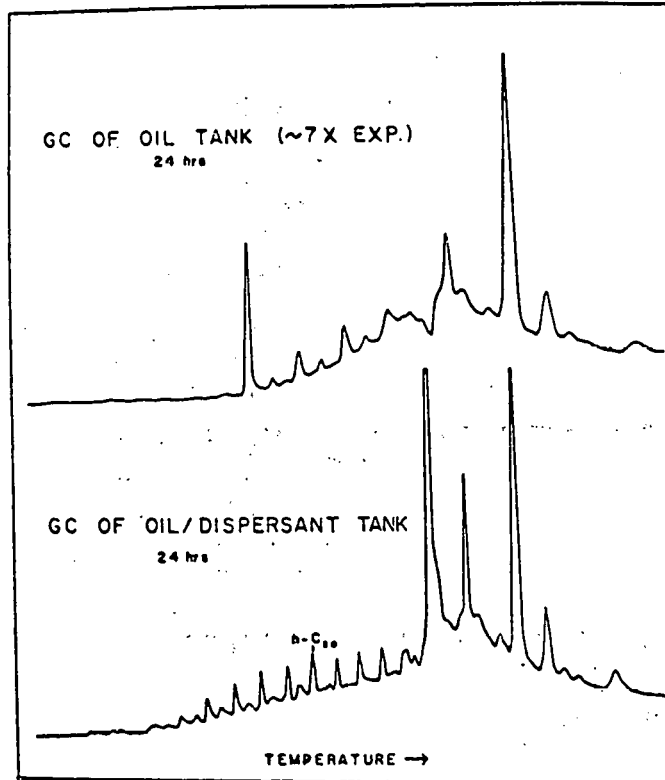


Figure 7.4.6 GC of the 24 Hour Top Samples from the Treated and Untreated Tanks

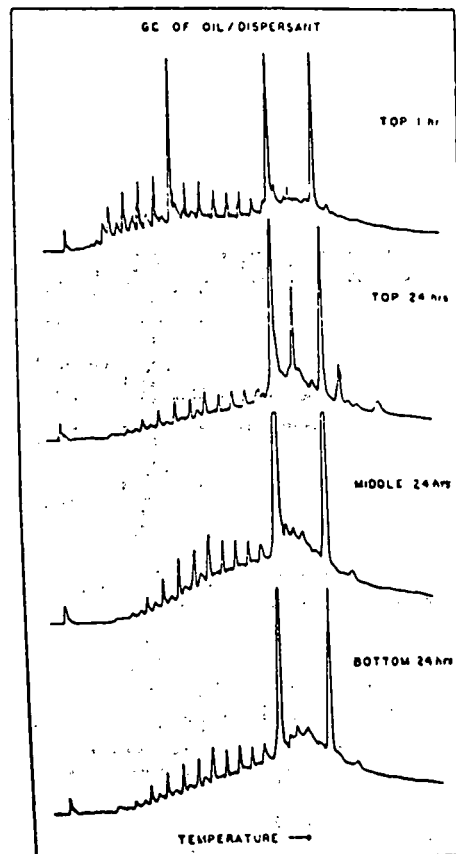


Figure 7.4.7 GC of Samples from the Treated Tank; 1 hr., top; 24 hrs., top; 24 hrs., middle; and 24 hrs., bottom (Exp. 2)

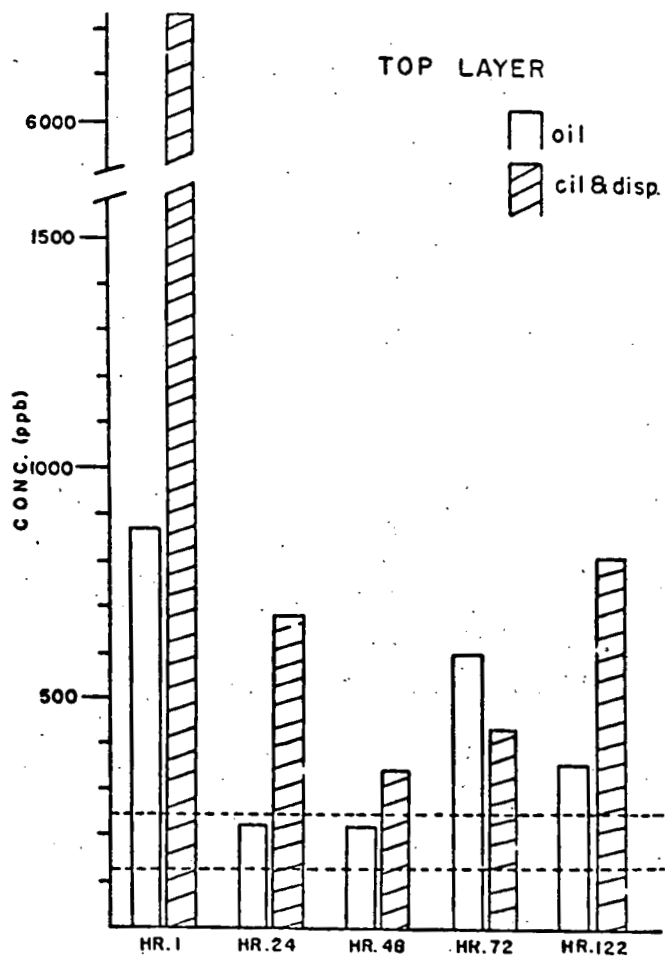


Figure 7.4.8 Concentrations of Extractable Organics from the Top (1 m) Port as a Function of Time. (Exp. 3)

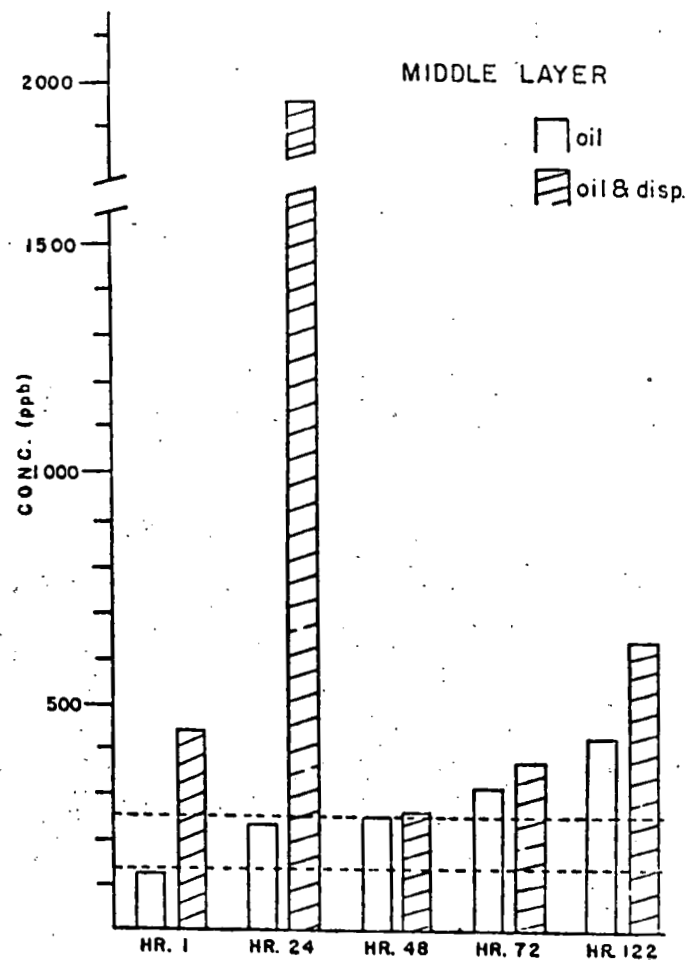


Figure 7.4.9 Concentrations of Extractable Organics from the Middle Port (3 m) as a Function of Time. (Exp. 3)

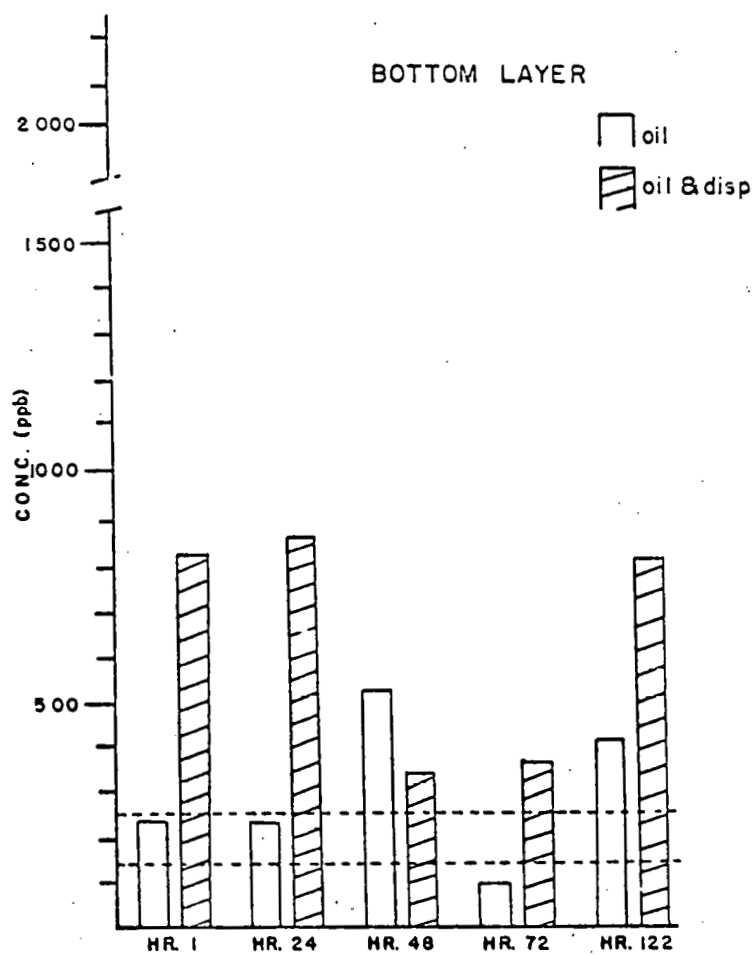


Figure 7.4.10 Concentrations of Extractable Organics from the Bottom Port (5.5 m) as a Function of Time. (Exp. 3)

The 1 and 24 hour values for the middle port are also similar to experiment 2 but, again, there is an abrupt decrease in concentration in the treated tank by the next sampling period. Samples from the bottom port of the treated tank were high at 1 hour and remained at this level for 24 hours before decreasing. However, the untreated tank had a high level at 48 hours, and then dropped to control level.

After 4 days, both tanks were agitated by stirring with a glass rod for 10 minutes, and samples were collected 24 hours later. The agitation increased the concentration at all levels.

(iv) Experiment 4:

The concentration of the top, middle and bottom layer as a function of time are shown in Figure 7.4.11, 7.4.12, and 7.4.13. In this experiment, the east control tank was used. The 1 hour concentration in the control tank was at least three times lower than previous experiments. However, the trend for the 24 to 72 hour samples was very similar to experiment 3. A very high concentration was detected in the middle port of the treated tank after 48 hours. The concentration at 1 hour was higher in other experiments, whereas the concentration at 24 hours was lower. The concentration in the bottom of the treated tank gradually increased with time. All concentrations in the untreated tank were at about the control level.

(v) Conclusions:

After only four completed experiments, it is too early to draw any definitive conclusions. The concentration values for experiment 2 seem to follow anticipated levels. For this reason, we undertook a complete analysis of all samples. The GC results shown in Figures 7.4.6 and 7.4.7 emphasize some of the major differences between the treated and untreated samples and changes of the treated samples with time and depth.

(b) Air Samples

For these experiments, 60 ml of Kuwait crude oil were added to the north and south tanks, and 12 ml of Corexit 9527 were then added to the south tank.

The surface was mixed for 10 minutes by stirring with glass rods. Air samples were collected immediately after the spill. Air samples were collected and treated similar to the air samples taken in the laboratory experiments. Figure 7.4.14 shows the system used for collecting the air samples in the meso scale experiments. The funnels through which the air was pumped were placed at about 2.5 cm above the water surface.

One experiment was conducted with the tanks covered to eliminate wind and rain effects. This was important to the water column measurements. The covers were made of wood and had four holes of 2.5 cm diameter for ventilation and one hole of about 20 cm in the center of the cover on which the funnel was placed. Prior to the addition of the oil, control samples were collected from above both tanks. Surface samples were taken and treated as in the laboratory experiments.

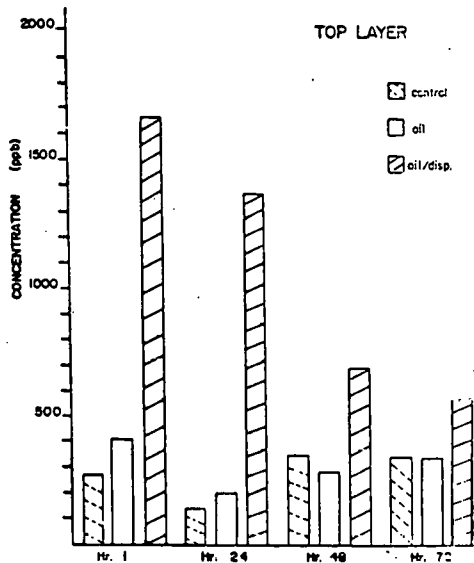


Figure 7.4.11 Concentrations of Extractable Organics from the Top Port (1 m) as a Function of Time. (Exp. 4)

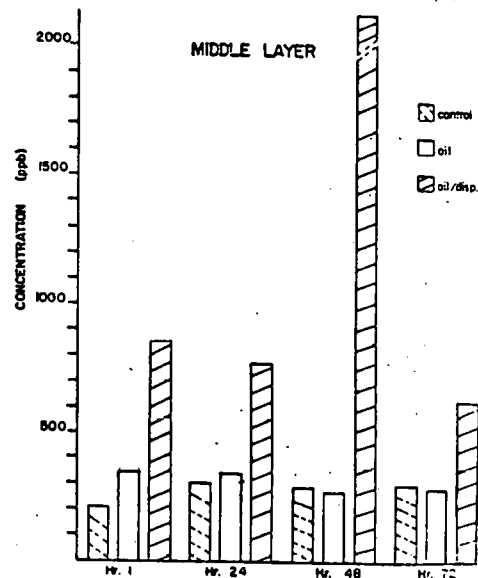


Figure 7.4.12 Concentrations of Extractable Organics from the Middle Port (3 m) as a Function of Time. (Exp. 4)

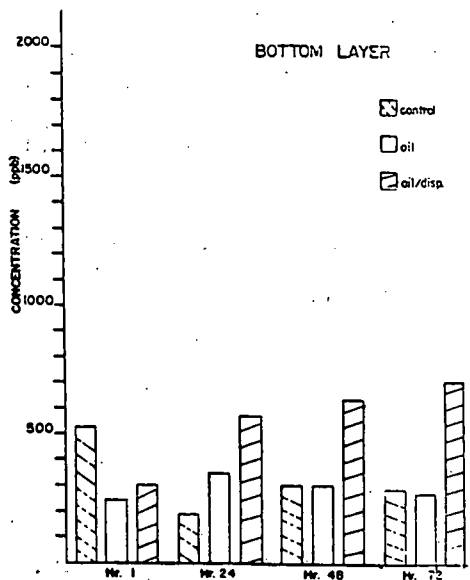


Figure 7.4.13 Concentrations of Extractable Organics from the Bottom Port (5.5 m) as a Function of Time (Exp. 4)

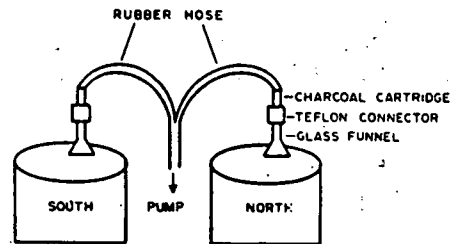


Figure 7.4.14 System Used to Collect Air Samples in the Meso Scale Experiments

The following experiments were performed:

(i) Experiment 1:

The water temperature at the beginning of the experiment was 24°C. Control samples were taken during the 1.5 hours before the oil was added. Air samples were taken at 0-3 and 3-6 hours. Surface samples were taken at 72 hours after the addition of the oil.

(ii) Experiment 2:

The water temperature was 19°C at the beginning of the experiment. Control samples were taken during 1 hour. Air samples were taken at 0-1.5, 1.5-4, and 4-7 hours. Surface samples were taken at 1.5, 4, 7, 48 and 72 hours after the spill.

(iii) Experiment 3

In this experiment, the tanks were covered with the wooden covers. The temperature at the beginning of the experiment was 10.5°C. Control samples were taken during 50 minutes. Air samples were collected at 0.3-5, 1.5-4, 4-7 and 7-20.5 hours. Surface samples were collected at 72 hours after the spill. An internal standard, n-C₂₀, was added after the IR measurements.

(iv) Results and Discussion

Experiment 1:

The air samples collected above both tanks were quite similar. The gas chromatograms of the air samples taken at 0-3 hours are shown in Figure 7.4.15 and those taken at 3-6 hours are shown in Figure 7.4.14. Samples taken at 3-6 hours indicated the presence of n-C₁₂ to n-C₁₆. All components lighter than n-C₁₂ evaporated from both treated and untreated slicks within 3 hours. The surface samples taken at 72 hours after the spill indicated that all the components up to n-C₁₆ disappeared from the treated and untreated slicks. The gas chromatograms of both surface samples were similar.

The IR spectra of both air samples taken at 3-6 hours indicated that the light aromatics, i.e., benzene, toluene and xylene, evaporated within 3 hours (or less) as their specific bands did not appear in the spectra (Figures 7.4.17 and 7.4.18).

Experiment 2:

All components up to n-C₁₆ appeared in the air samples of the treated and untreated spills taken at 0-1.5 hours. Gas chromatograms of samples taken at 1.5-4 hours showed the presence of n-C₁₁-n-C₁₇ in both air samples. All components up to n-C evaporated within 1.5 hours. The gas chromatograms of the air samples at 4-7 hours, shown in Figure 7.4.19 indicated the presence of n-C₁₂-n-C₁₇ in the oil air sample and n-C₁₃-n-C₁₇ in the oil and dispersant air sample.

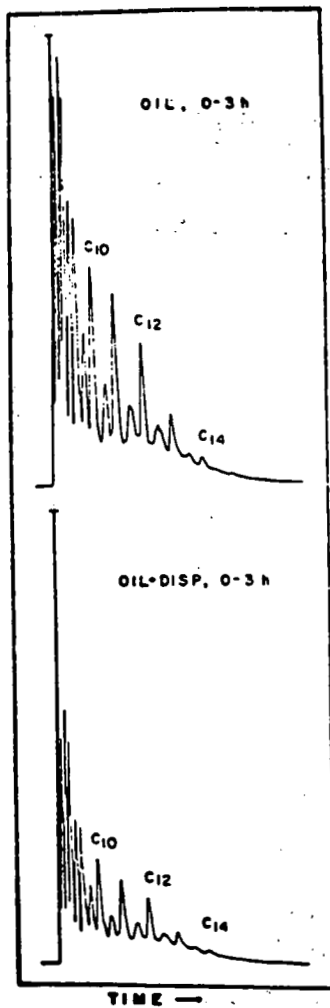


Figure 7.4.15 GC of the Air Samples Collected at 0-3 Hours (Meso Scale Exp. 1)

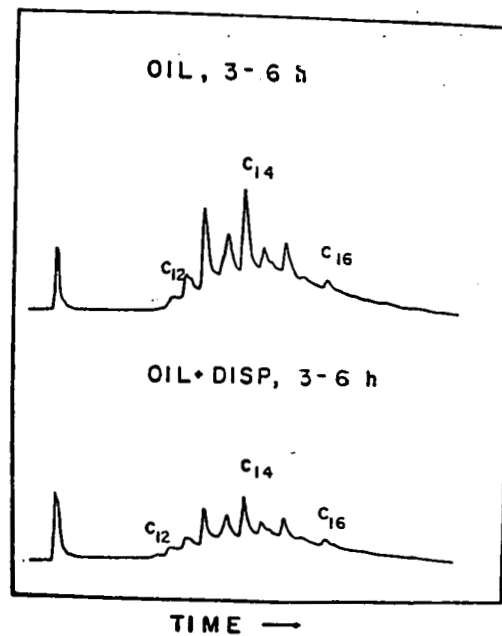


Figure 7.4.16 GC of the Air Samples Collected at 3-6 Hours (Meso Scale Exp. 1)

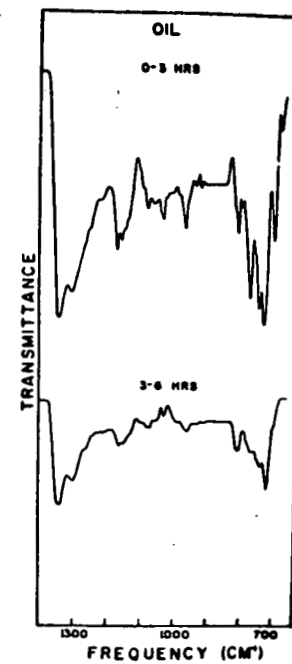


Figure 7.4.17 IR Spectra of the Oil Air Samples Collected at 0-3 and 3-6 Hrs. (Meso Scale Exp. 1)

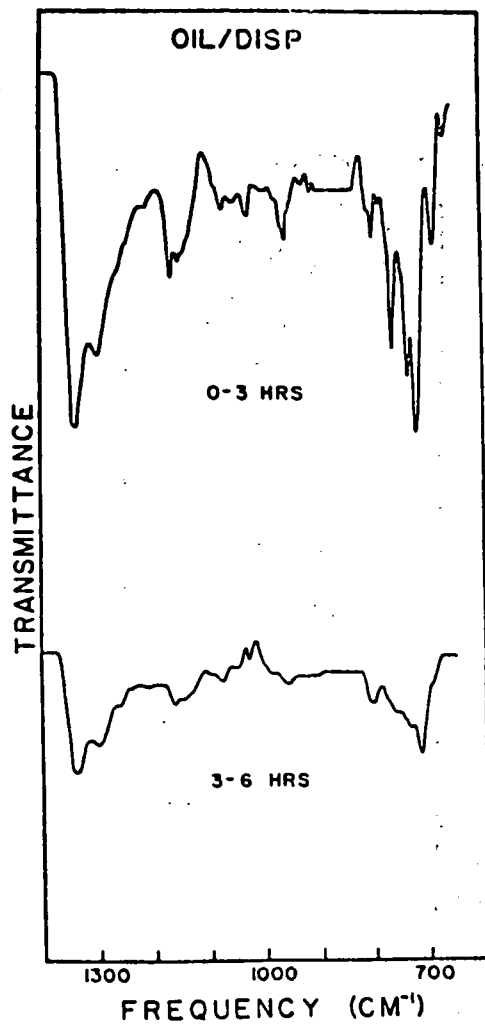


Figure 7.4.18 IR Spectra of the Oil + Dispersant Air Samples Collected at 0-3 and 3-6 Hrs. (Meso Scale Exp. 1)

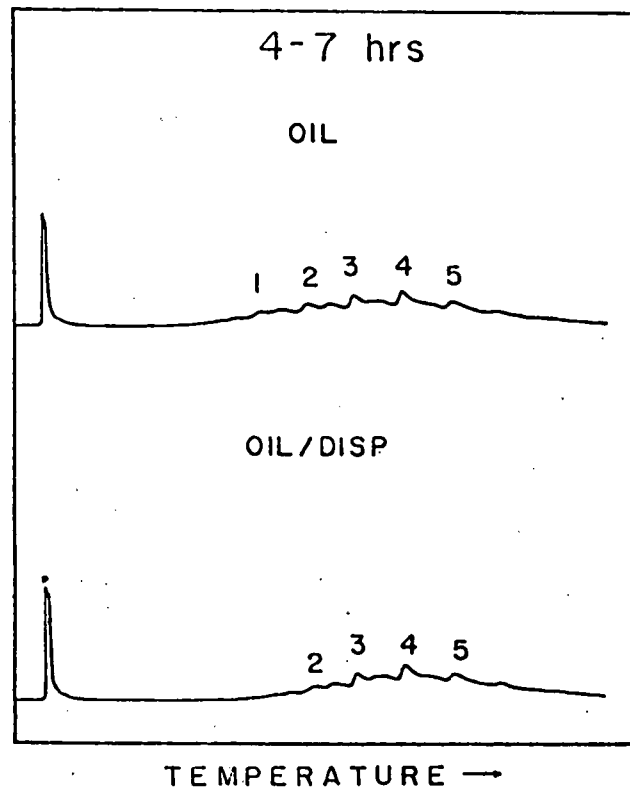


Figure 7.4.19 GC of the Air Samples Collected at 4-7 Hrs. (Meso Scale Exp. 2)

A surface sample from the oil slick taken at 1.5 hours indicated that all hydrocarbons up to $n\text{-C}_{10}$ had disappeared. The oil and dispersant slick sample taken at the same time indicated that all components lighter than $n\text{-C}_{11}$ had disappeared (Figure 7.4.20). The relative amount of $n\text{-C}_{10}$ in the oil slick sample was small and this might be the reason why it did not appear in the air sample taken at 1.5-4 hours above the oil slick, which was more dilute than the surface sample.

Samples from both slicks taken at 4 and 7 hours after the spill indicated that the lightest hydrocarbon present was $n\text{-C}_{12}$, but the treated slick contained relatively less amounts of $n\text{-C}_{12}$ and $n\text{-C}_{13}$. $n\text{-C}_{13}$ was present in the untreated slick sample taken at 48 hours after the spill, but disappeared from the treated slick (Figure 7.4.21). Surface samples of both slicks taken at 72 hours after the spill showed that all hydrocarbons lighter than $n\text{-C}_{14}$ had disappeared. The results obtained from the air samples are in agreement with the results obtained from the surface samples. The evaporation was slightly faster from the treated slick.

The IR spectra of the air samples taken at 1.5-4 hours showed that benzene, toluene, and xylene disappeared within 1.5 hours from both spills.

Experiment 3:

This experiment was performed with covers on the tanks as described in the experimental section. The evaporation was slower than in the open tank experiments, as expected. The control air samples indicated the presence of some organics in the air, but their amount was negligible compared to the vapors collected. Figure 7.4.22 shows the relative heights of the GC peaks of the n -alkanes at different times. The evaporation rate of the n -alkanes was slightly faster in the treated slick. However, the difference does not seem to be significant.

Figure 7.4.23 shows the IR spectra of the air samples taken at 0.3-1.5 hours. The benzene band at 670 cm^{-1} does not appear in either air sample, indicating that the benzene evaporated within 20 minutes (it took 20 minutes to stir the surface and to cover the tanks). Surface samples taken at 72 hours after the spill indicated that all hydrocarbons lighter than $n\text{-C}_{14}$ disappeared from the treated and untreated slicks.

c) Conclusions:

The meso scale experiments indicated that the difference between the evaporation rates of the n -alkanes from the treated and untreated slicks were small. One experiment showed no difference and the other two showed a slightly faster evaporation from the treated slick. Oil vs. oil experiments were not performed in the meso scale, so it is difficult to conclude whether the differences were due to the dispersant or to experimental errors.

Results of the meso scale experiments were in agreement with the laboratory scale experiments when mixing was not applied. Evaporation was faster in the meso scale (open tank) experiments because of the wind. The mixing that was applied in the meso scale experiments, i.e.,

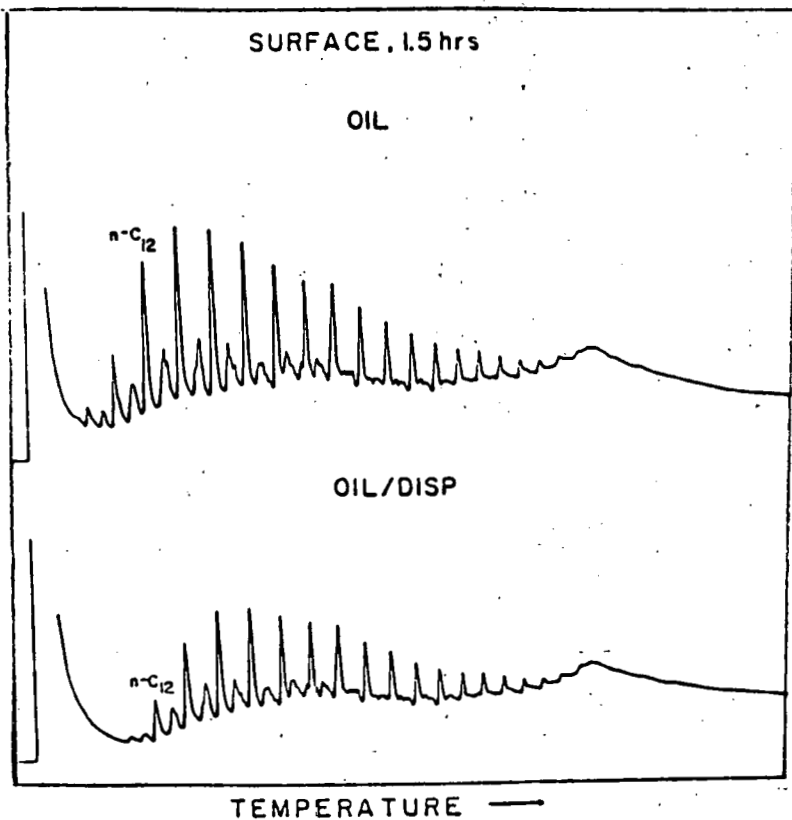


Figure 7.4.20 GC of Surface Samples Collected 1.5 Hours After the Spill (Meso Scale exp. 2)

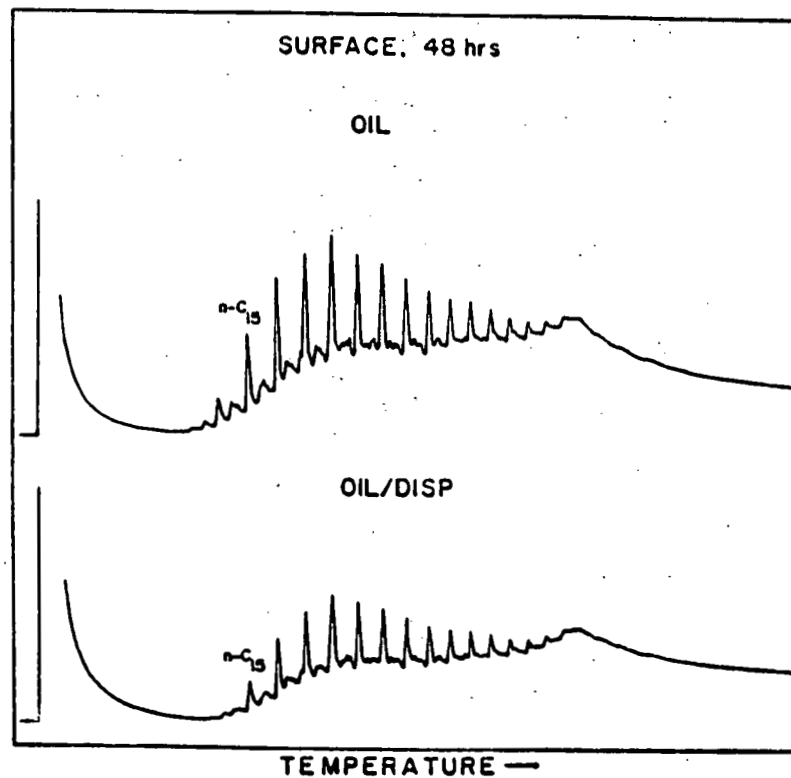


Figure 7.4.21 GC of Surface Samples Collected 48 Hours After the Spill (Meso Scale Exp. 2)

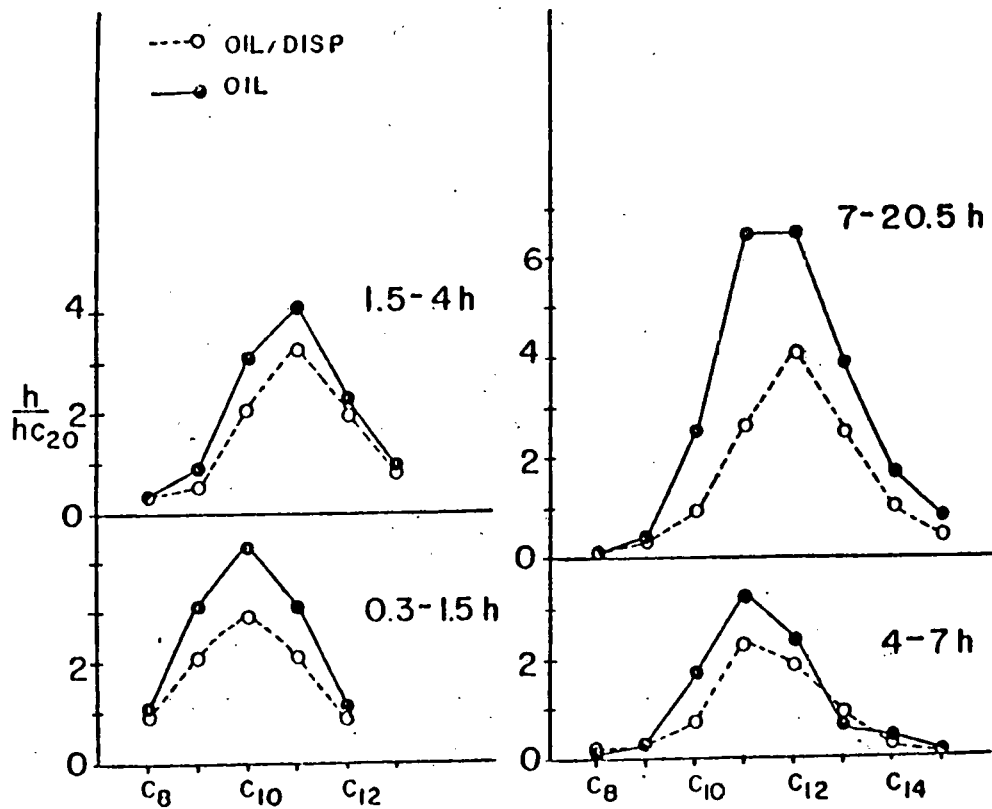


Figure 7.4.22 Relative GC Peak Heights of the n-alkanes as a Function of the Carbon Number. (meso scale Experiment 3, Air samples Taken at 0.3-1.5, 1.5-4, 4-7, and 7-20.5 hrs)

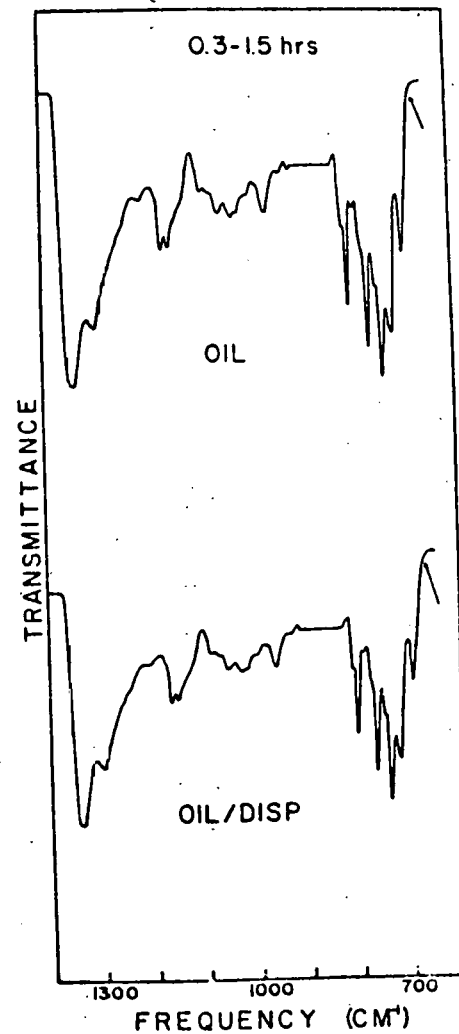


Figure 7.4.23 IR Spectra of the Air Samples Collected at 0.3-1.5 Hrs. (Meso Scale Experiment 3)

The arrows show the position of the benzene band.

stirring with glass rods, seemed to be inefficient in affecting the evaporation rates of the light n-alkanes. The wall effect that was mentioned in the laboratory experiments also exists in the tanks and could cause some differences in the effects of the dispersants on evaporation between meso scale experiments and open sea experiments.

(B) Series II

This series of experiments tested various modes of application of oil and dispersant to the seawater in the meso scale tanks. The water temperature remained a relatively constant 21°C throughout the 6 experiments. Amounts of oil and/or dispersant added to the tanks as well as the mode of application are listed in Table 7.4.1. The first experiment was run for 72 hours whereas the remaining experiments were conducted for 24 hours each. At each sampling period, 1 liter water samples were collected and returned to this laboratory for quantitative infrared analysis. Table 7.4.2 a & b presents results for each experiment and the discussion of each follows:

(a) Water Analysis

(i) Experiment 1:

Control levels of approximately 100 ppb were found for all levels and sampling periods in the control (east) tank except for the middle layer at 48 hours). This value was close to the bay level (131 ppb). The highest concentrations of hydrocarbons are found in the middle layer of the south tank after 1 hour. The north tank had a relatively even distribution of hydrocarbons which is twice the control level but after 24 hours, amounts close to the control level were reached in this tank and in the south tank. For this reason, the remaining experiments were conducted for a 24 hour duration.

(ii) Experiment 2:

In this experiment, the amount of oil and dispersant added to the tank was increased while the ratio of oil:dispersant was kept to 5:1. Application was also the same as in experiment 1. Table 7.4.2b shows that the hydrocarbon levels and distribution in the north tank after 1 hour are almost identical to those in the first experiment, i.e., increasing the oil in the north tank did not increase the amount entering the water column. In the south tank, overall amounts of hydrocarbons and their relative distribution is the opposite to the first experiment. The top and middle layer increased after the first hour, while their relative distribution is the opposite in the first experiment in these two layers. The hydrocarbons do not seem to reach the bottom layer during this time.

After 24 hours, hydrocarbon levels in the north tank have increased slightly over those in the 1 hour sampling. In the south tank overall levels are still high and the distribution among layers again corresponds with the first experiment.

Table 7.4.1

Exp. #	Tank	Kuwait (ml)	Dispers. (ml)	Mode of Application of Dispersant	Comments
1	8/1/78 North	60	12	premixed w/ 120 ml sea water/sprayed on	sprayed*
	South	60			sprayed
2	8/16/78 North	300	60	premix. w/600 ml. seawater/sprayed on	sprayed
	South	300			sprayed
3	8/22/78 North	60	12	premix. w/120 ml freshwater/sprayed on	sprayed
	South	60			sprayed
4	8/28/78 North	300	60	poured no premix.	sprayed
	South	300			sprayed
5	8/31/78 North	60	12	premix. w/oil poured	sprayed
	South	60			sprayed
6	9/6/78 North	60	12	premix. w/oil & 120 ml. fresh water poured	sprayed
	South	60			sprayed

*Indicates a spray of salt water over surface of "spill."

Table 7.4.2b Infrared Quantitative Analysis (ppb)

Mr. #	Sample Location	Tank N	S	E
Exp. 2 1	Top	216	98,918	105
	Mid	120	46,227	105
	Bot	326	301	107
	Ct*	184	265	
24	Top	326	11,279	326
	Mid	212	9,753	106
	Bot	319	672	219
Exp. 3 1	Top	223	1,614	102
	Mid	283	1,578	101
	Bot	231	129	112
	Ct	219	417	
24	Top	110	395	298
	Mid	105	993	407
	bot	212	399	322
Exp. 4 1	Top	330	36,525	333
	Mid	219	17,462	109
	Bot	474	694	245
	Ct	323	441	112
24	Top	330	6,122	260
	Mid	218	6,089	106
	Bot	168	2,978	110
Exp. 5 1	Top	268	23,228	241
	Mid	345	22,549	223
	Bot	327	2,376	219
	Ct	354	1,590	185
24	Top	854	7,988	323
	Mid	769	7,680	330
	Bot	670	15,650	272
Exp. 6 1	Top	326	6,852	214
	Mid	237	1,271	353
	bot	330	3,999	234
	Ct	218	1,578	280
24	Top	452	5,420	210
	Mid	447	4,709	306
	bot	457	2,363	223

*Ct - control

Table 7.4.2a Infrared Quantitative Analysis (ppb)

Mr. #	Sample Location	Tank N	S	E
1	top	223	951	-
	mid	110	1336	108
	bot	232	672	105
24	top	214	527	108
	mid	221	384	105
	bot	0	403	543
48	top	105	133	0
	mid	109	132	691
	bot	121	285	113
72	top	-	403	213
	mid	107	256	104
	bot	102	267	167
CONTROL		0	135	110
BAY	131			

(iii) Experiment 3:

In this series, the mode of application of dispersant was changed by premixing it with fresh water instead of sea water as in the last two experiments. The amount of oil and/or dispersant was reduced to the levels of the first experiment.

Taking into consideration the level of the controls for the north and south tank, levels of hydrocarbons parallel those of the first experiment after the first hour with highest concentrations in the south tank remaining in the top and middle layers. After twenty-four hours, levels in the north tank decreased slightly whereas levels in the south tank decreased significantly, approaching control values in top and bottom layers. The concentration in middle layer is about double that of the control.

The fresh water application seems to mix the oil/dispersant further into the depth of the tank but after 24 hours, the patterns of mixing resembles that of the sea water premix experiments.

(iv) Experiment 4:

The dispersant/oil amount was increased to experiment 2 levels. The dispersant was not premixed in this case, but was poured directly onto the oil in the tank. This was followed by a spray with water over the surface. As can be seen from Table 7.4.2b, the hydrocarbon levels in the north tank are consistent with those of previous experiments. In the south tank overall hydrocarbon levels after one hour correspond to those in experiment 2; however, the top layer in this case, contains the highest level. This would indicate that premixing the dispersant with water does aid in the incorporation of the oil/dispersant complex to a greater depth in the water column.

After 24 hours, the south tank has the highest concentration in the top two layers while the bottom layer is relatively low, but contains more organics than is evidenced in previous experiments.

(v) Experiment 5:

Oil and dispersant were premixed and poured on the water in the south tank. Both north and south were then sprayed with additional water. The control in the south tank indicates residual oil/dispersant which may have not been thoroughly removed from the tank prior to this experiment. Taking this into consideration, the comparatively high level of hydrocarbon in the bottom layer can be explained. After one hour, the levels of hydrocarbon in the top and middle layers of the south tank are among the highest detected in any of the six experiments, although only 60 mls. oil/12 mls. dispersant were added originally. After 24 hours, the highest level in the south tank was detected in the bottom layer.

(vi) Experiment 6:

The dispersant (12ml) was premixed with oil and fresh water prior to pouring onto the water surface of the south tank. The highest concentration of organics was found in the top layer of the south tank after one hour. After 24 hours, the top and middle layer have about the same amounts of hydrocarbons; however, the levels in this experiment are an order of a magnitude less than those in the previous experiment.

GC/MS analysis was performed on samples from experiment 2. In the north tank, components were below detectable limits (Table 7.4.3). The 1 hour samples in the south tank contained detectable amount of all aromatic components listed except for benzene. Normal hydrocarbons ranged between C₁₀ to C₁₈ for the top layer and C₁₁ to C₁₈ for the middle layer. The predominant peak in the top layer was C₁₂, whereas the higher boiling C₁₄ dominated in the middle layer. After 24 hours, xylene was lost in both layers. The middle layer also lost naphthalene. The normal alkane range remained the same for the top layer, but the predominant peak was the higher boiling C₁₄. In the middle layer the predominant peak remained C₁₄ but the low alkane shifted from C₁₁ to C₁₂. GC/MS of deasphalted Kuwait oil contains all aromatics listed in Table 7.4.3 and has a n-C_n range of C₉-C₁₈ with the predominant peak occurring at C₁₀.

(vii) Conclusions:

Effectiveness of the dispersant in carrying the oil into the water column is proportional to the amount of contact of the dispersant with both the polar water fraction and the non-polar oil fraction of the oil/water system. The most intimate contact between these fractions was achieved when the dispersant was premixed with the oil. In all experiments, agitation of the water surface in the tanks also aided in mixing the oil/dispersant complex into the water column. The north tank showed little, if any, increase over control values during the course of the six experiments. In the south tank, the highest concentration of hydrocarbons was found generally in the top and middle layers after 1 hour, with a relative reduction in concentration after 24 hours (in some cases reduction to control levels). The level of hydrocarbons in the south tank was determined more by the mode of dispersant application than by amount of oil/dispersant added.

GC/MS spectra and infrared values seem to indicate that after 24 hours there is an overall loss of organics from the water column and since this loss, as indicated by GC/MS, is in the more volatile components, it seems fair to conclude that these lighter components may be lost to the atmosphere.

(C) Series III

Because of the high level of residual organics detected in the south tank, both tanks were thoroughly cleaned and a second series of 5 twenty-four hour experiments were conducted. The mode of application of oil and/or dispersant as well as amounts of both are listed in Table 7.4.4. Quantitative infrared results are listed in Table 7.4.5 and are

TABLE 7.4.3

<u>SAMPLE</u>	<u>BENZENE</u>	<u>XYLENES</u>	<u>NAPHTHALENE</u>	<u>METHYL-NAPH.</u>	<u>DIMETHYL-NAPTH.</u>	<u>n-Cn RANGE</u>	<u>(PREDOMINANT PEAK)</u>
S-TOP-1hr.(99ppm)		X	X	X	X	C ₁₀ thru C ₁₈	C ₁₂
S-TOP-24hr.(11ppm)			X	X	X	C ₁₀ thru C ₁₈	C ₁₄
S-MID-1hr.(46ppm)		X	X	X	X	C ₁₁ thru C ₁₈	C ₁₄
S-MID-24hr.(10ppm)				X	X	C ₁₂ thru C ₁₈	C ₁₄
S-CTRL(0.2ppm)	BELOW DETECTABLE						
N-TOP-1hr.(0.2ppm)	LIMITS						
N-TOP-24hr.(0.3ppm)	"						
N-MID-1hr.(0.1ppm)	"						
N-MID-24hr.(0.2ppm)	"						
N-CTRL(0.2ppm)	"						
KUWAIT CRUDE (DEASPHALTED)	X	X	X	X	X	C ₉ thru C ₁₈	C ₁₀

SUMMARY OF RESULTS FOR GC/MS/CS ANALYSIS FOR TANK EXPERIMENT 8/16/78

Table 7.4.4

<u>Exp. #</u>	<u>Tank</u>	<u>Kuwait (ml)</u>	<u>Disper. (ml)</u>	<u>Mode of Application of Dispersant</u>	<u>Comments</u>
1	10/13/78 North	60			sprayed salt
	South	60	12	premix. w/oil poured	sprayed salt
2	10/17/78 North	60			sprayed salt
	South	60	12	premix. w/oil & 120 ml fresh water; poured	sprayed salt
3	10/24/78 North	60			fresh water sprayed
		60	3	premix. w/120 ml fresh water; sprayed on	
4	10/30/78 North	160			fresh water sprayed
	South	160	32	premix. w/320 ml fresh water; sprayed on	
5	11/2/78 North	160			fresh water sprayed
		160	8	premix. w/120 ml fresh water; sprayed on	

Table 7.4.5 Infrared Quantitative Analysis (ppb)

Hr #	Sample Location	Tank N	S
Exp. 1	Ct	102	300
	Top		295
	Mid		214
1	Top	339	22,201
	Mid	229	20,168
	Bot	292	101
24	Top	729	15,684
	Mid	88	14,888
	Bot	81	712
Exp. 2	Ct	100	79
	Top		81
	Mid		82
1	Top	250	30
	Mid	148	1,325
	Bot	250	511
24	Top	245	45,734
	Mid	358	26,837
	Bot	306	719
Exp. 3	Ct	388	144
	Top		145
	Mid		84
1	Top	258	935
	Mid	345	893
	Bot	206	513
24	Top	268	519
	Mid	288	553
	Bot	371	513
Exp. 4	Ct	324	383
	Top		234
	Mid		379
1	Top	293	2,848
	Mid	261	2,286
	Bot	176	1,533
24	Top	322	935
	Mid	316	1,506
	Bot	391	1,246
Exp. 5	Ct.	327	210
	Top		305
	Mid		371
1	Top	412	1,118
	Mid	237	559
	Bot	237	675
24	Top	375	709
	Mid	687	771
	bot	326	876

discussed below:

(a) Water Analysis

(i) Experiment 1:

A 5:1 oil to dispersant ratio was used, the oil being mixed with the dispersant prior to pouring the mixture in the south tank. Both north and south tanks were then sprayed with salt water. The results show that the very high concentrations of organics are found in the top and middle layer after 1 hour with a slight reduction after 24 hours. The bottom layer has relatively little organics even after 24 hours. The north tank shows very little change in hydrocarbon level throughout the experiment.

(ii) Experiment 2:

The ratio and amount of oil was maintained as in Experiment 1. However, the dispersant was premixed with fresh water and oil prior to pouring on the south tank. Both north and south tanks were subsequently sprayed with salt water. In the south tank after 1 hour a substantial increase in organics occurs in the middle layer while an almost non-detectable amount is seen in the top layer. The bottom layer increases slightly over that in the first experiment. An unusual occurrence is seen after 24 hours, when the top and middle layer increase substantially to levels which occurred in previous experiments only after the first hour.

(iii) Experiment 3:

The ratio of oil:dispersant was decreased to 20:1 and the dispersant was premixed with fresh water prior to spraying on the oil slick in the south tank. In this case, the levels of hydrocarbons in the south tank greatly decreased while migration of organics was deeper into the water column than previously seen.

(iv) Experiment 4:

The amount of oil/dispersant was premixed with fresh water and this mixture was sprayed on the slick. This method of premixing and spraying seemed to promote deeper penetration of organics into the south tank, with the highest levels at the top, but comparatively high levels through to the bottom. This is the first experiment showing such penetration. After twenty-four hours, the middle and bottom layers contain the highest organic concentration.

(v) Experiment 5:

In this experiment the dispersant was decreased to yield a 20:1 oil/dispersant ratio. The dispersant was premixed with fresh water and this mixture was sprayed onto the slick. Overall concentrations in the water column are lower, but the depth of penetration parallels the previous experiment.

(vi) Conclusions:

The mode of application which causes the highest concentrations of organics in the overall water column is the one which premixes oil/dispersant or oil/water/dispersant prior to adding to the water in the south tank. Depth of penetration of organics into the tank is greatest for the dispersant which is sprayed on the tanks. The controlling factor in concentration of organics seems to be premixing of oil/dispersant rather than mode of application or amounts of oil/dispersant added.

(D) Series IV Meso-Scale Flow-thru Experiment

Two experiments (referred to as Trial 1 and Trial 2) were performed using the meso-scale tank equipped with a flow-thru system. Three tanks were used as follows:

- 1) control
- 2) 300 ml of Kuwait Oil
- 3) 300 ml of Kuwait Oil and 30 ml of Corexit 9527

One liter water samples were collected from the top, middle and bottom ports.

(i) Trial 1:

Quantitative results for the first trial experiment (aborted) at the meso scale tanks are given in Table 7.4.6 and GC's of selected samples are shown in Figures 7.4.24. and 7.4.28. The quantitative results indicate (and this is supported by the GC results) that oil entered the water column when the dispersant was used; however, after 24 hours the concentrations dropped to about three times that of the control. Very little chemical information was gained from an experiment of this short duration.

(ii) Trial 2:

(1) Quantitative Analysis

The amounts of extractable organics as determined by infrared spectroscopy are given in Table. 7.4.7. The values for the control tanks are all below 340 ppb except for the middle and bottom sampling ports at 350 hours. The values for the oil tank are in this same range until 48 hours when a larger amount was observed. The maximum value of 29,020 ppb was reached at 192 hours. The values for samples from the oil/dispersant tank are initially high for the top and middle of the tank; however, with time, the higher concentration migrates to the bottom. At 350 hours the only significantly high concentration is for samples from the bottom port of the tank.

(2) Qualitative Analysis

Control Tank:

Gas chromatograms (GC) of all samples having significant concentrations were measured. GC's of samples from the control tank are shown in Figures 7.4.29 - 7.4.40. Most of these chromatograms contain a series of peaks as shown in Figure 7.4.31, although they may contain additional

Table 7.4.6 Concentration (ppb) of extractable Organics in Water Samples from Flow-thru Tank Experiments at Narragansett bay Campus (Trial 1)

	Hours	0	1	24
(1) Control,	Top		270	185
	Mid	382	239	148
	Bot		280	193
(2) Oil,	Top		204	227
	Mid	414	230	216
	Bot		206	195
(3) Oil/Disp,	Top		2075	668
	Mid	458	3953	623
	Bot		247	240

Table 7.4.7 Concentrations (ppb) of extractable Organics in Water Samples from Flow-thru Tank Experiments at Narragansett Bay Campus (Trial 2)

	Hours	0	1	24	48	72	192	350
(1) Control,	Top		153	178	237	190	286	110
	Mid	340	102	200	185	261	105	1,386
	Bot		183	186	160	211	249	3,007
(2) Oil,	Top			232	1021	480	29,020	76.4
	Mid	308	162	273	325	309	1,851	192
	Bot		150	157	267	229	540	966
(3) Oil/Disp,	Top		54,276	9,776	5,486	3,706	2,638	264
	Mid	445	44,179	13,195	3,286	5,066	891	402
	Bot		294	265	1,516	4,006	11,939	1,033

Figure 7.4.24 GC of Surface Oil after 24 hrs. (Trial 1)

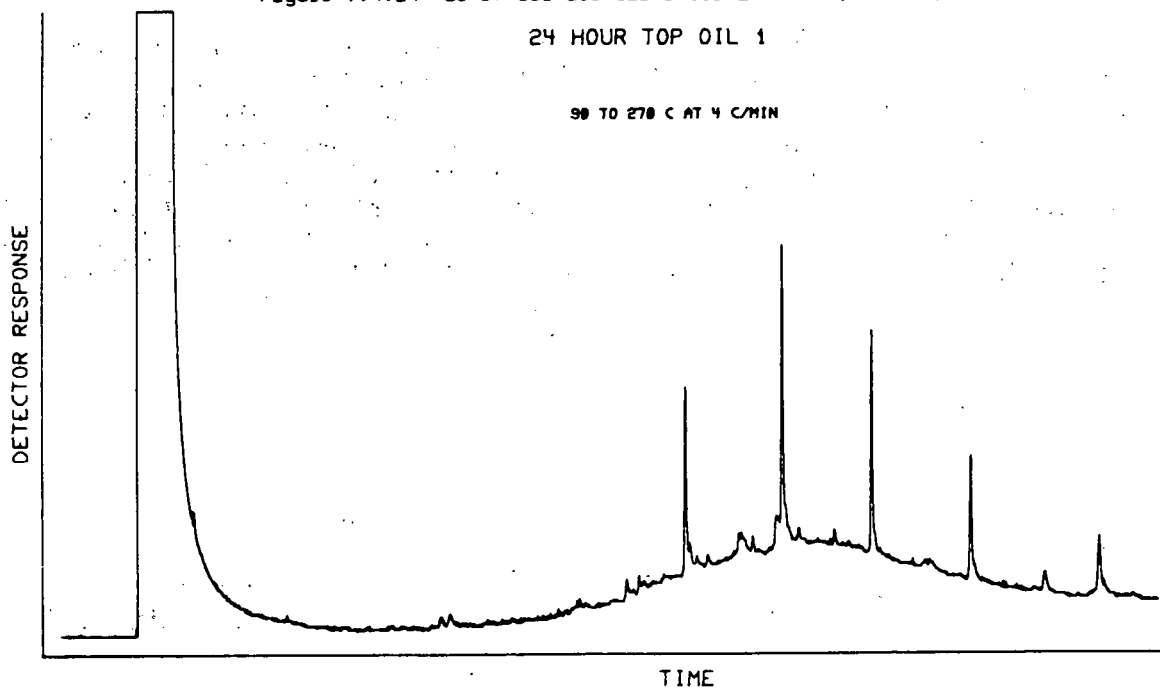


Figure 7.4.25 GC of Surface Oil/Dispersant after 1 hr. (Trial 1)

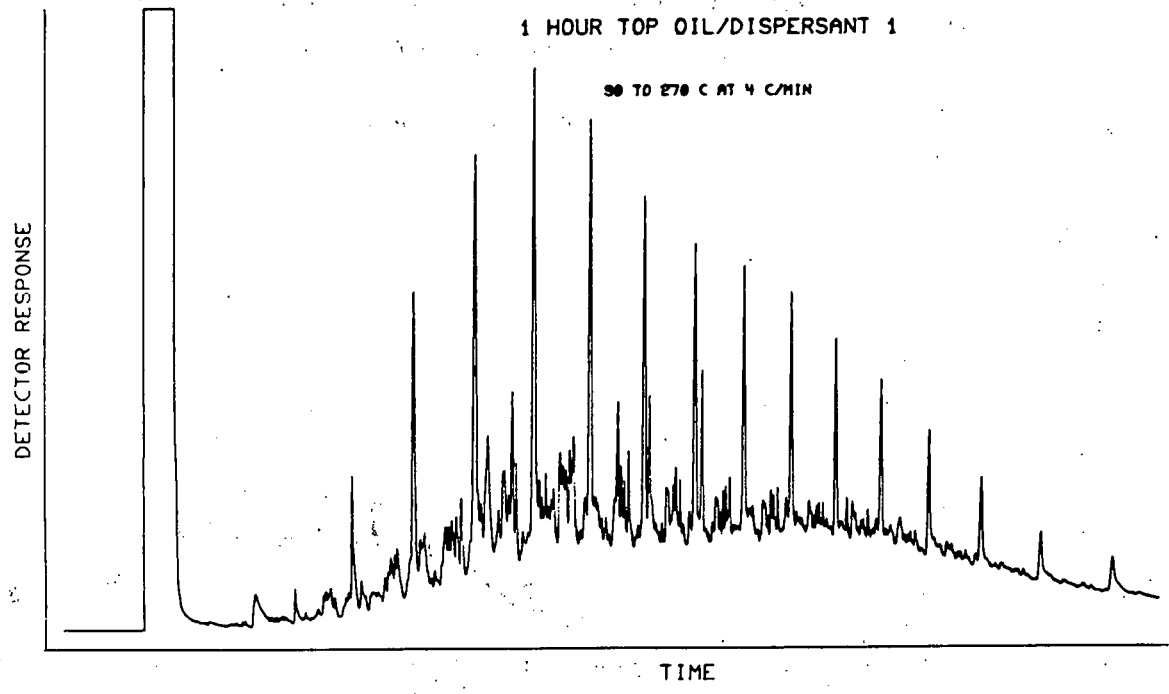


Figure 7.4.26 GC of Middle Oil/Dispersant after 1 hr. (Trial 1)

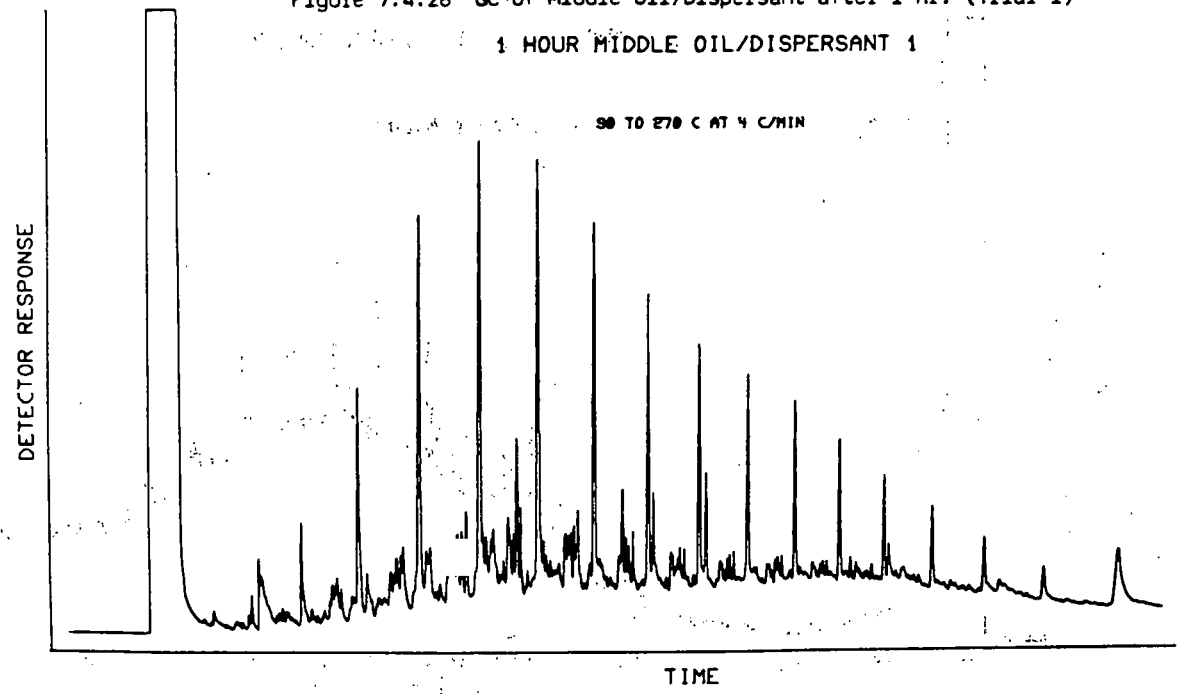


Figure 7.4.27 GC of Top Oil/Dispersant after 24 hrs. (Trial 1)

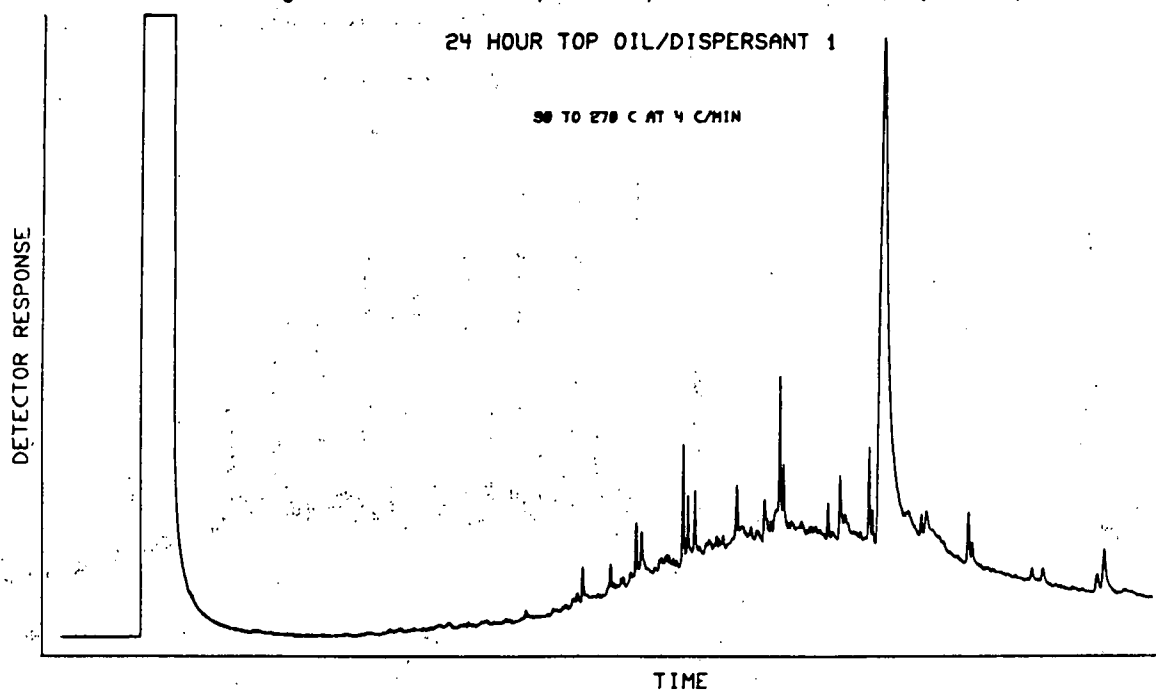


Figure 7.4.28 GC of Middle Oil/Dispersant after 24 hrs. (Trial 1)

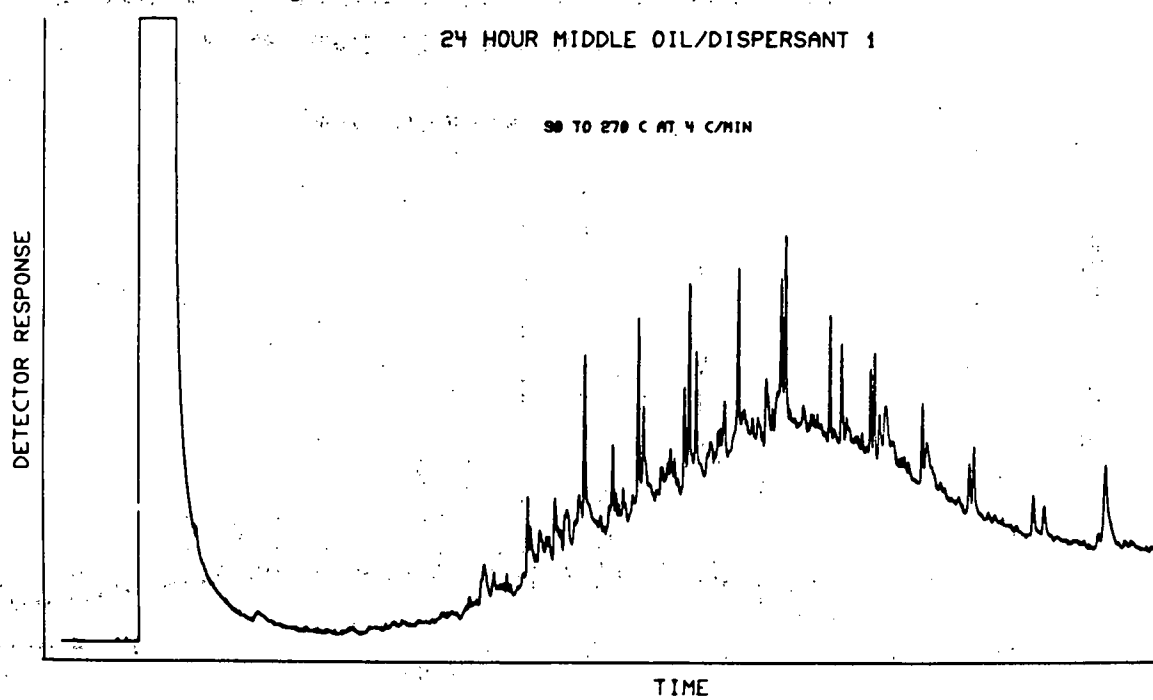


Figure 7.4.29 GC of Middle Control at 0 hr. (Trial 2)

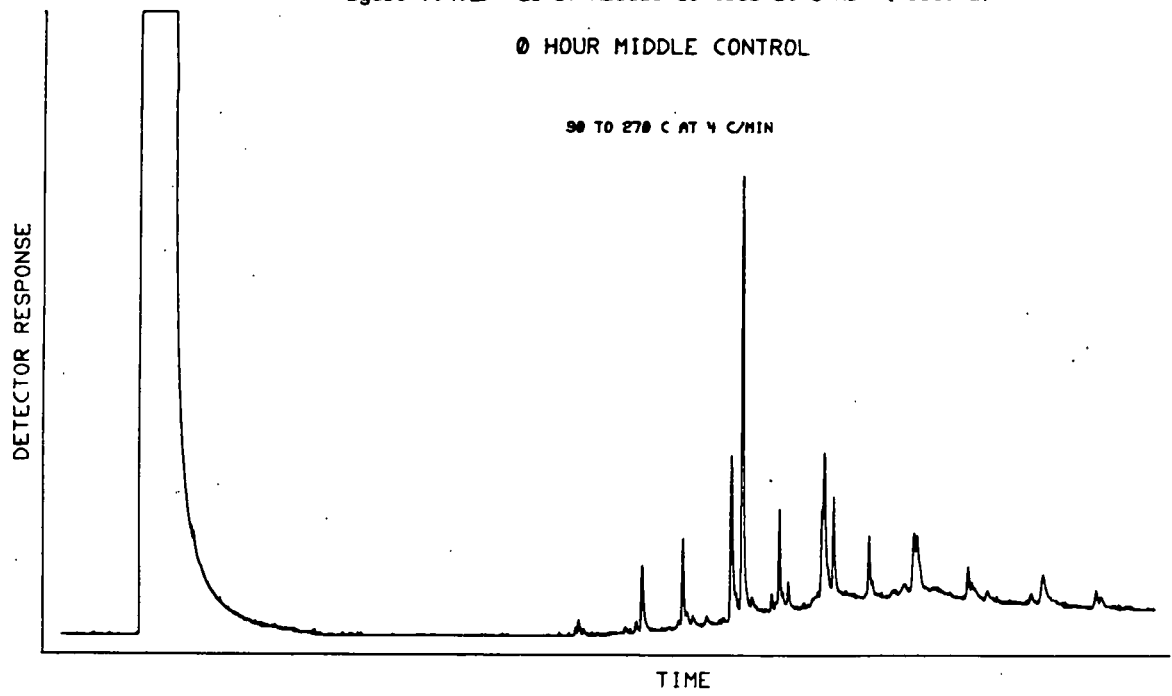


Figure 7.4.30 GC of Top Control after 1 hr. (Trial 2)

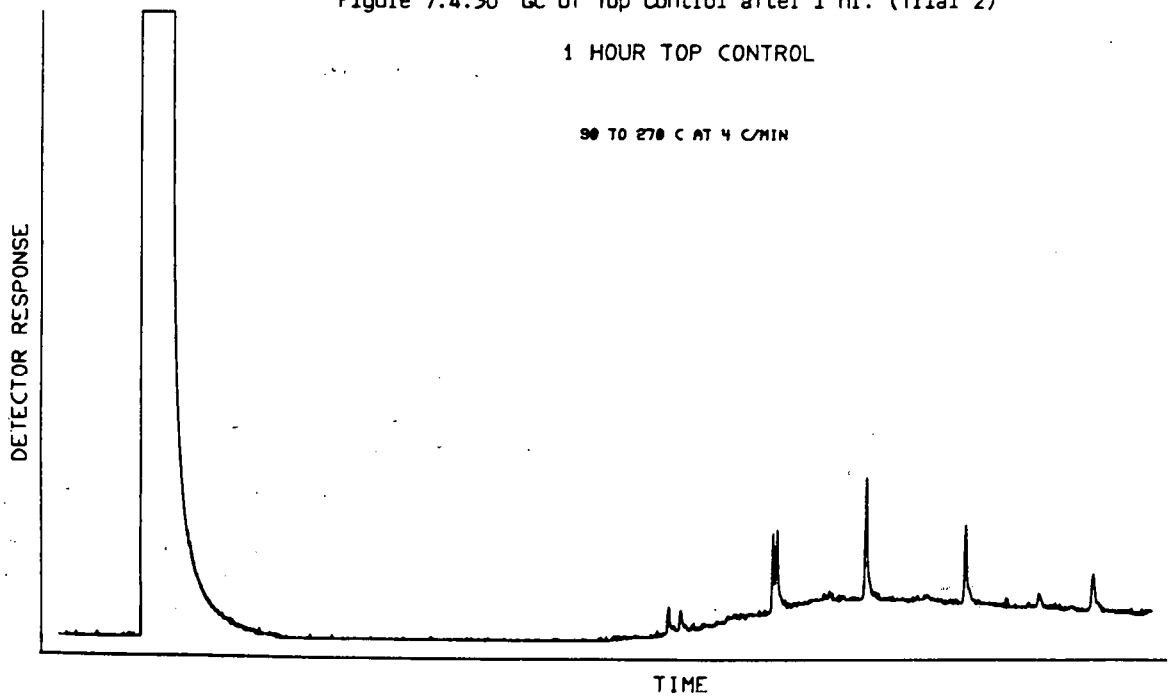


Figure 7.4.31 GC of Bottom Control after 1 hrs. (Trial 2)

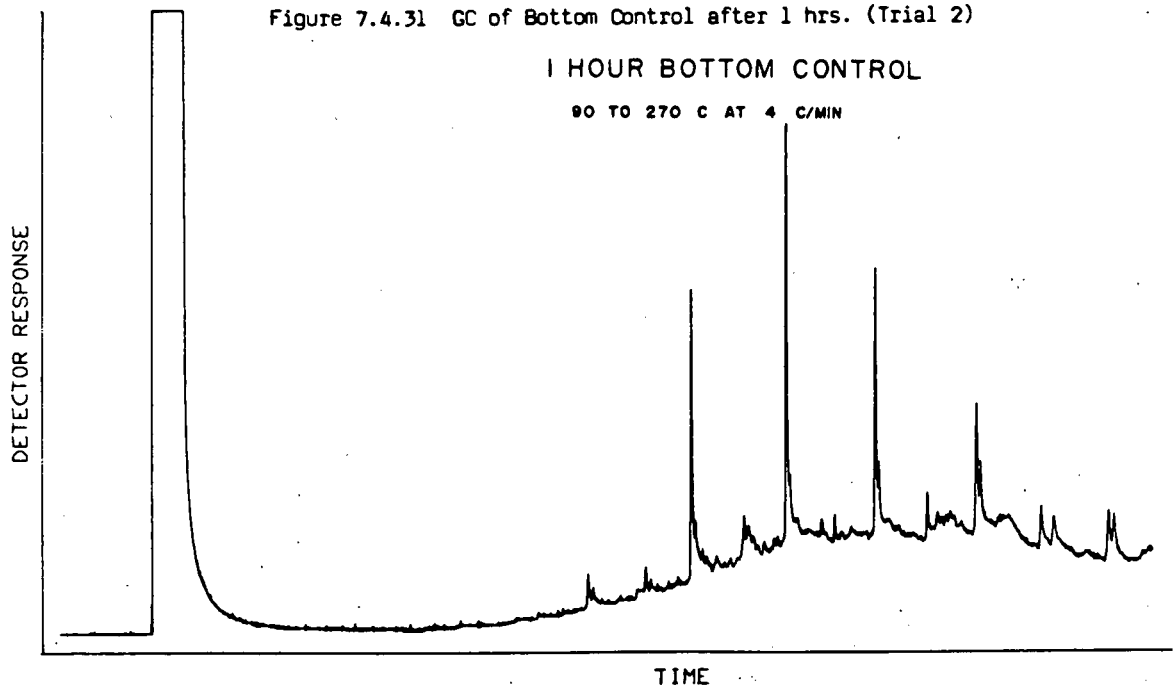


Figure 7.4.32 GC of Top Control after 48 hrs. (Trial 2)

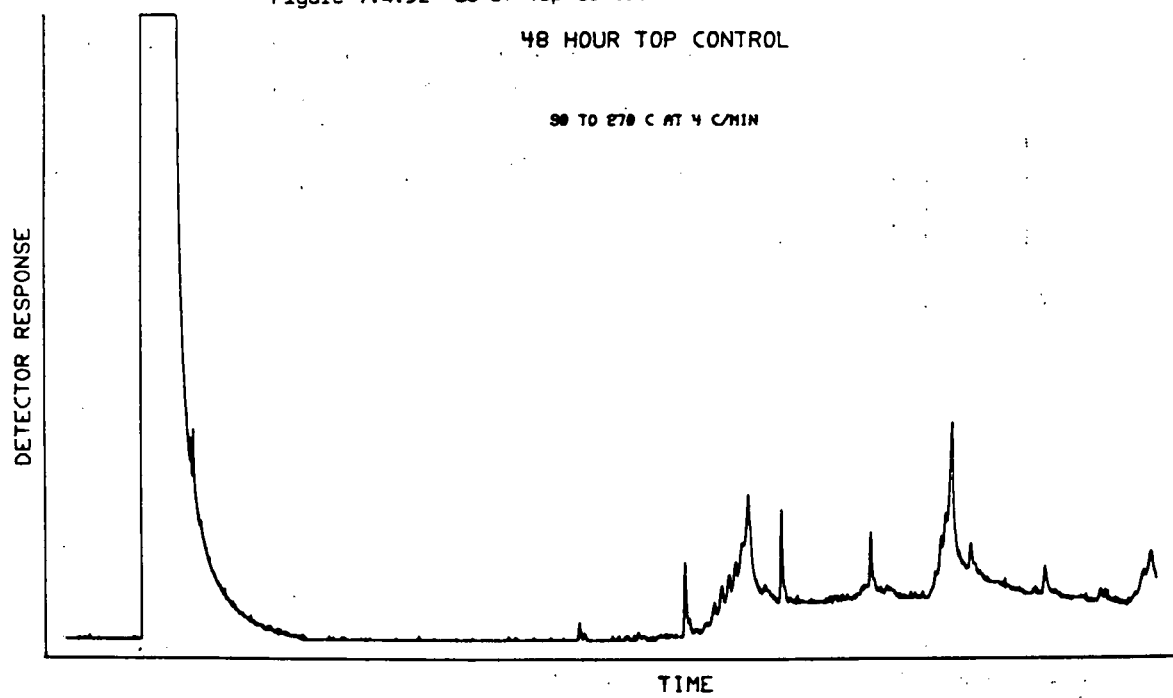


Figure 7.4.33 GC of Middle Control after 48 hrs. (Trial 2)

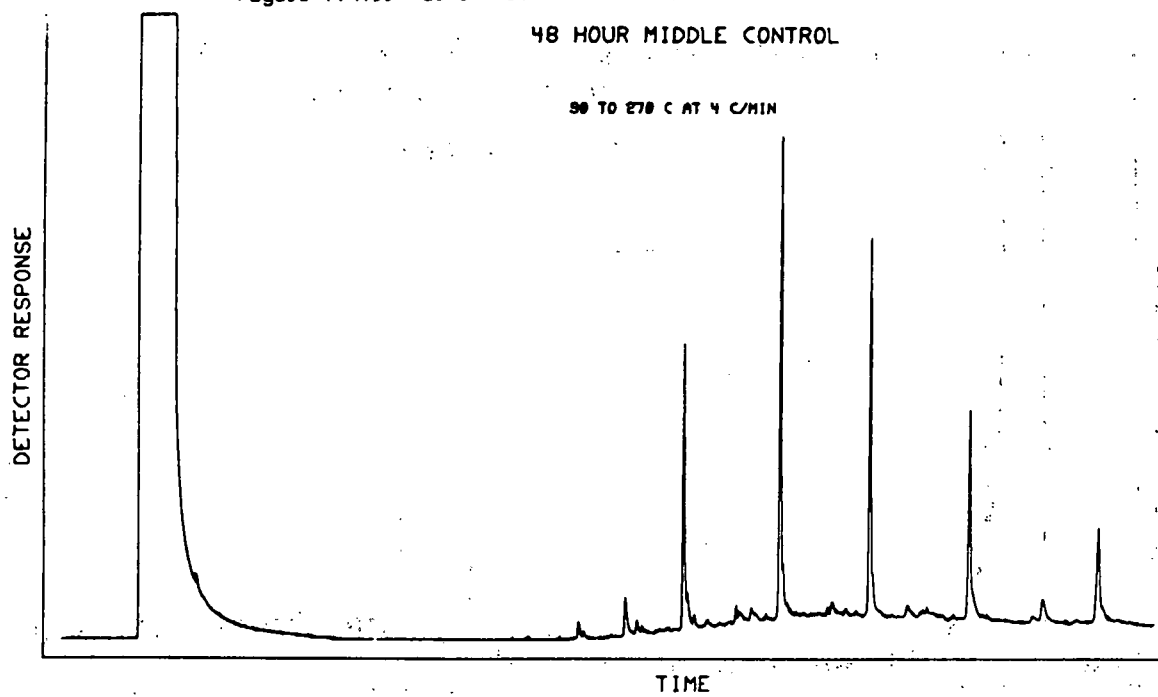


Figure 7.4.34 GC of Top Control after 72 hrs. (Trial 2)

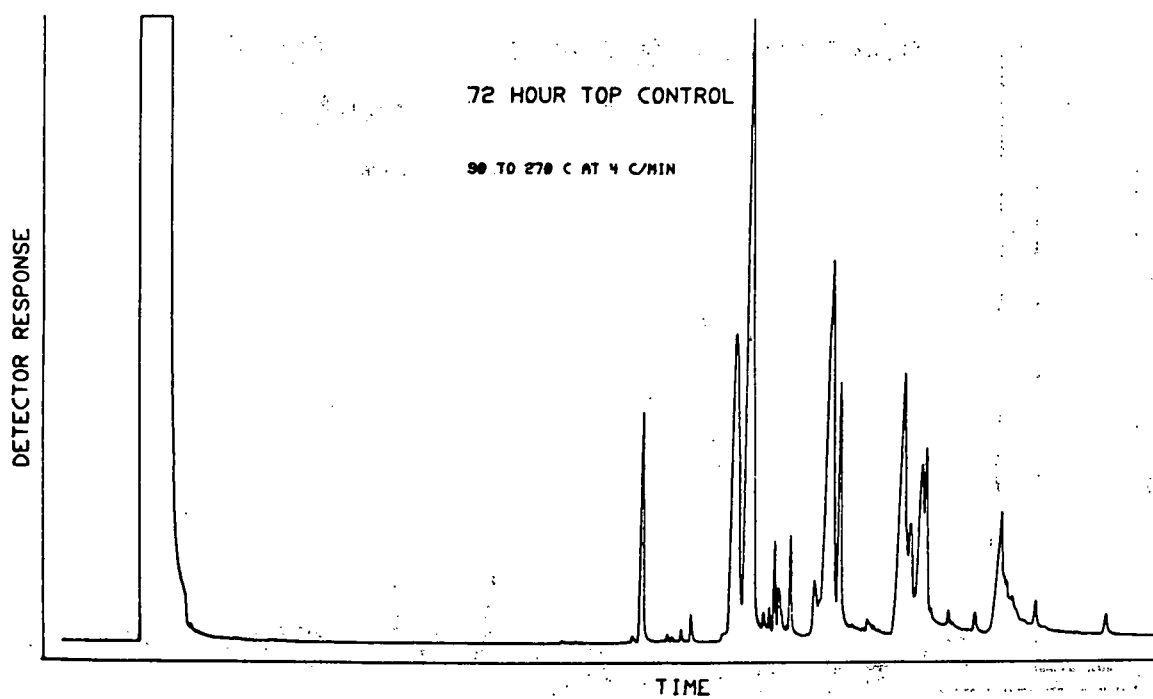


Figure 7.4.35 GC of Bottom Control after 72 hrs. (Trial 2)

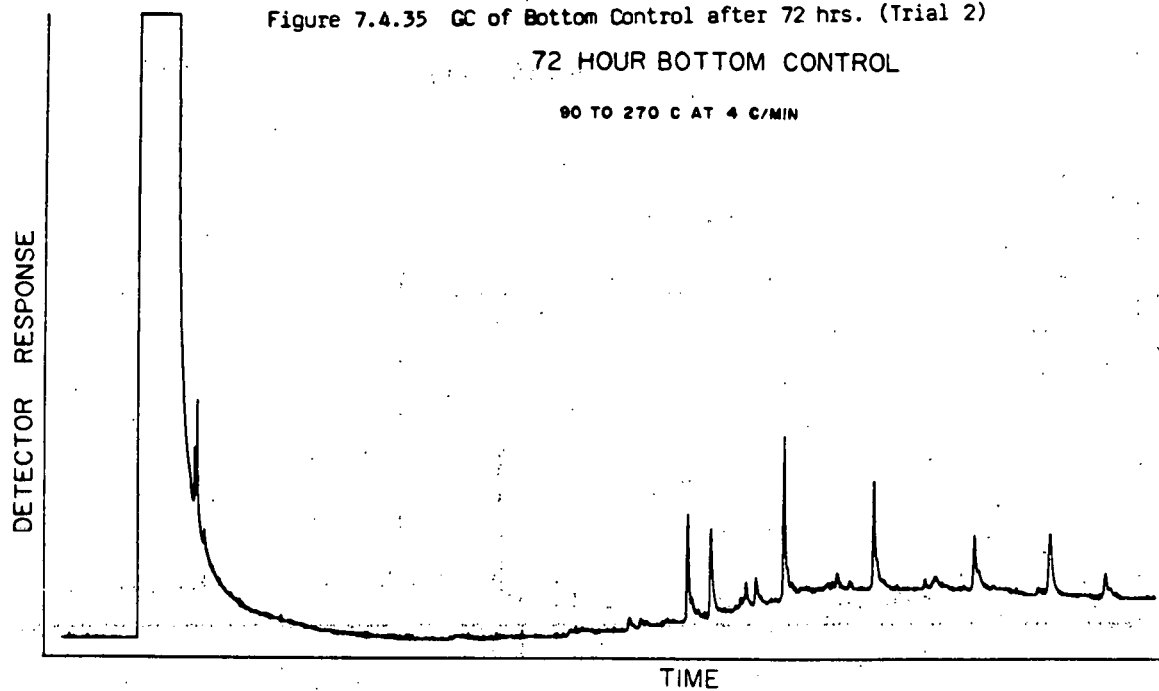


Figure 7.4.36 GC of Top Control after 192 hrs. (Trial 2)

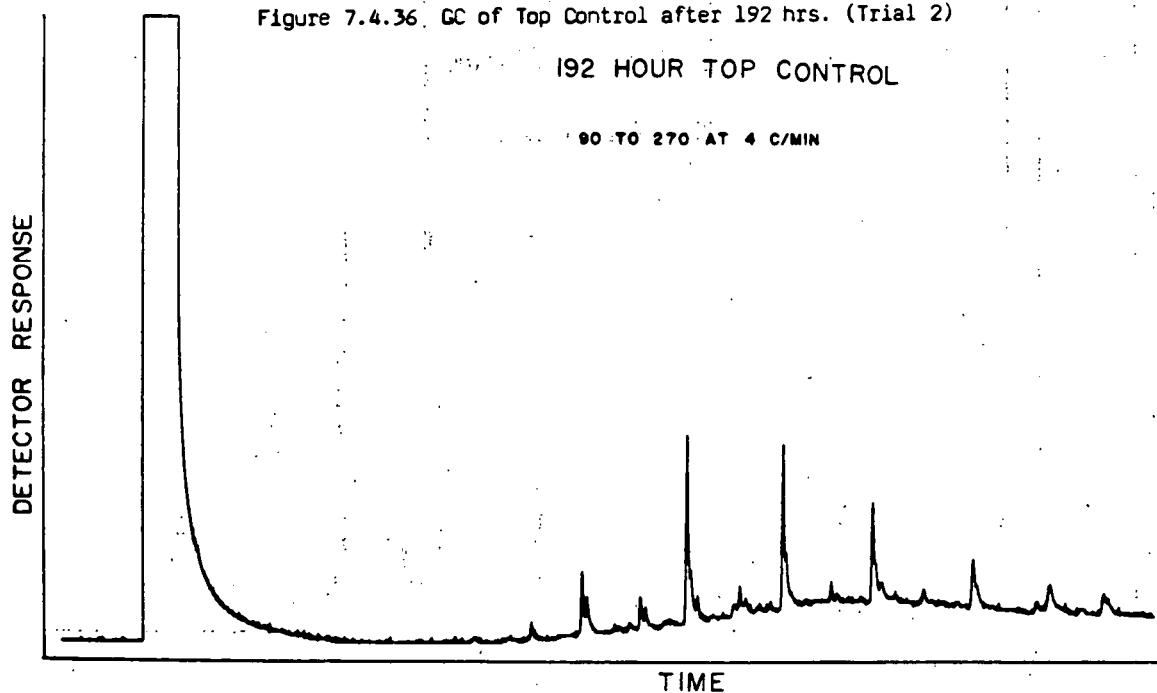


Figure 7.4.37 GC of Bottom Control after 192 hrs. (Trial 2)

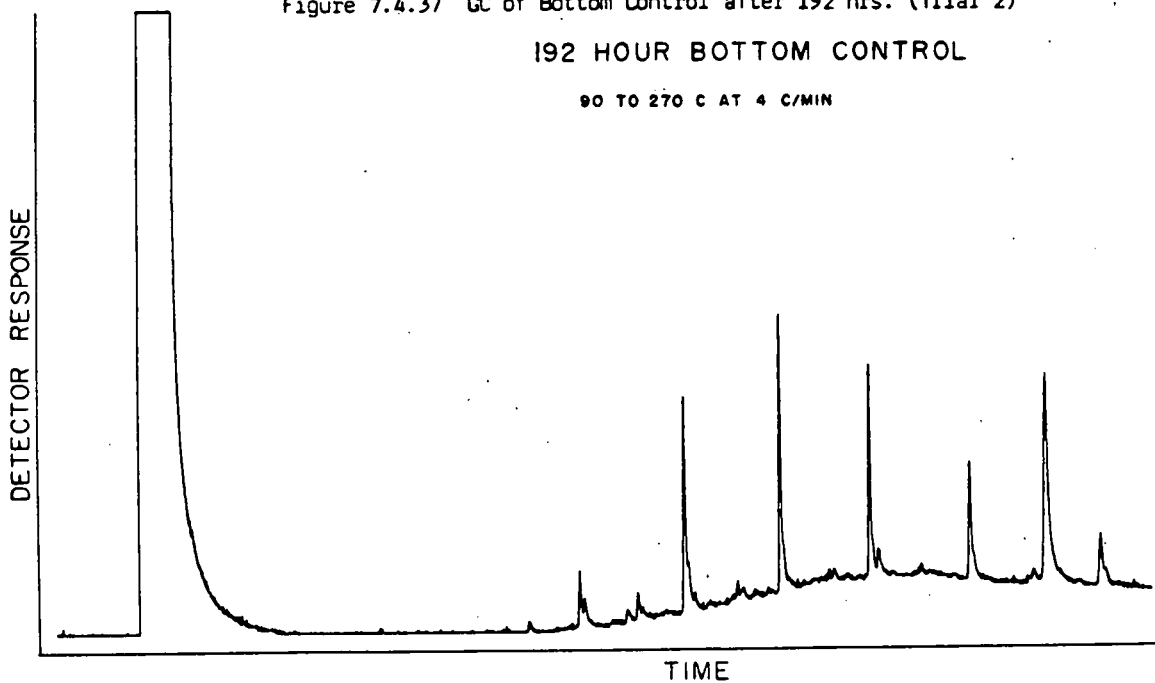


Figure 7.4.38 GC of Top Control after 350 hrs. (Trial 2)

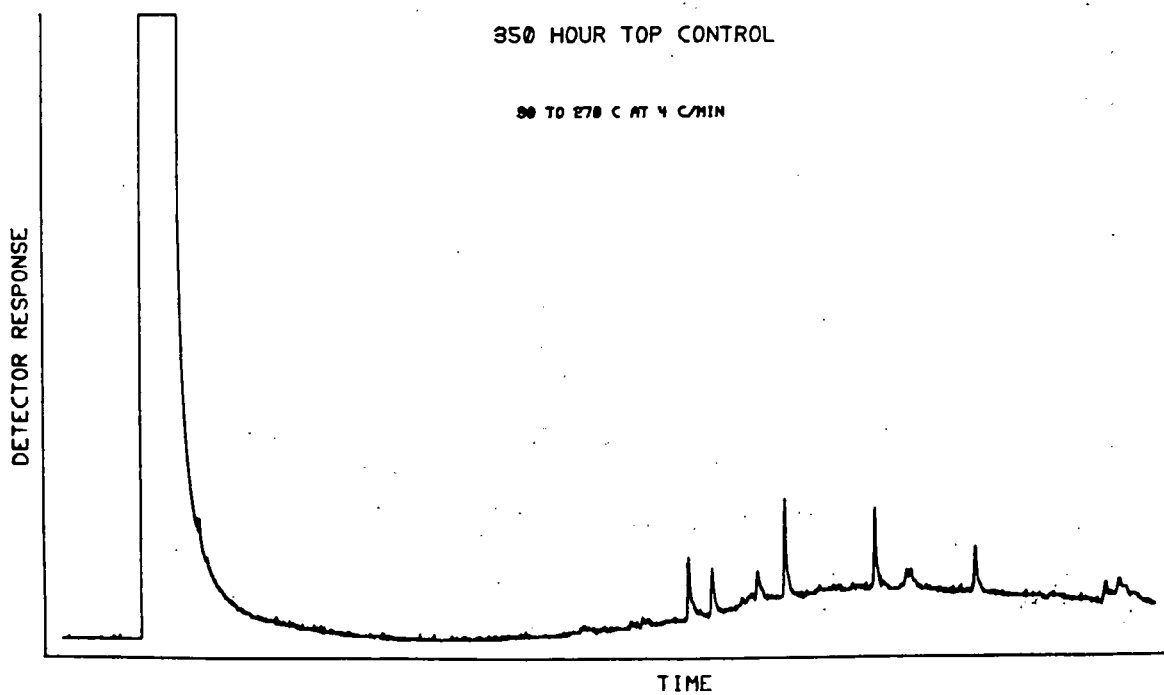


Figure 7.4.39 GC of Middle Control after 350 hrs. (Trial 2)

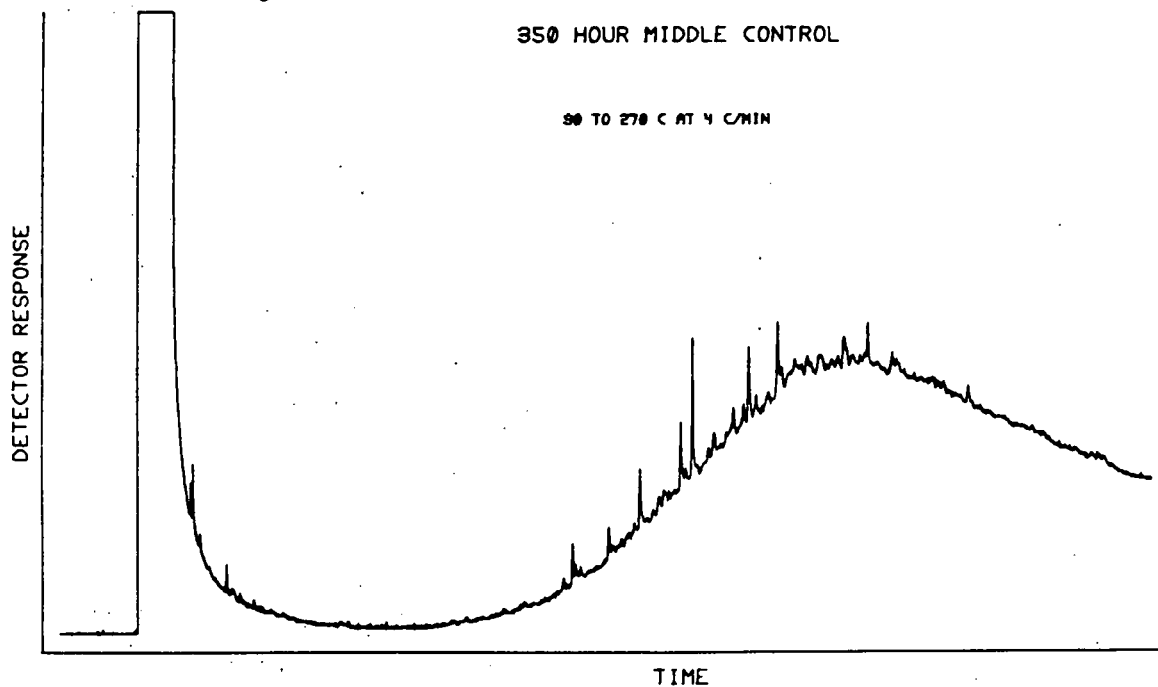
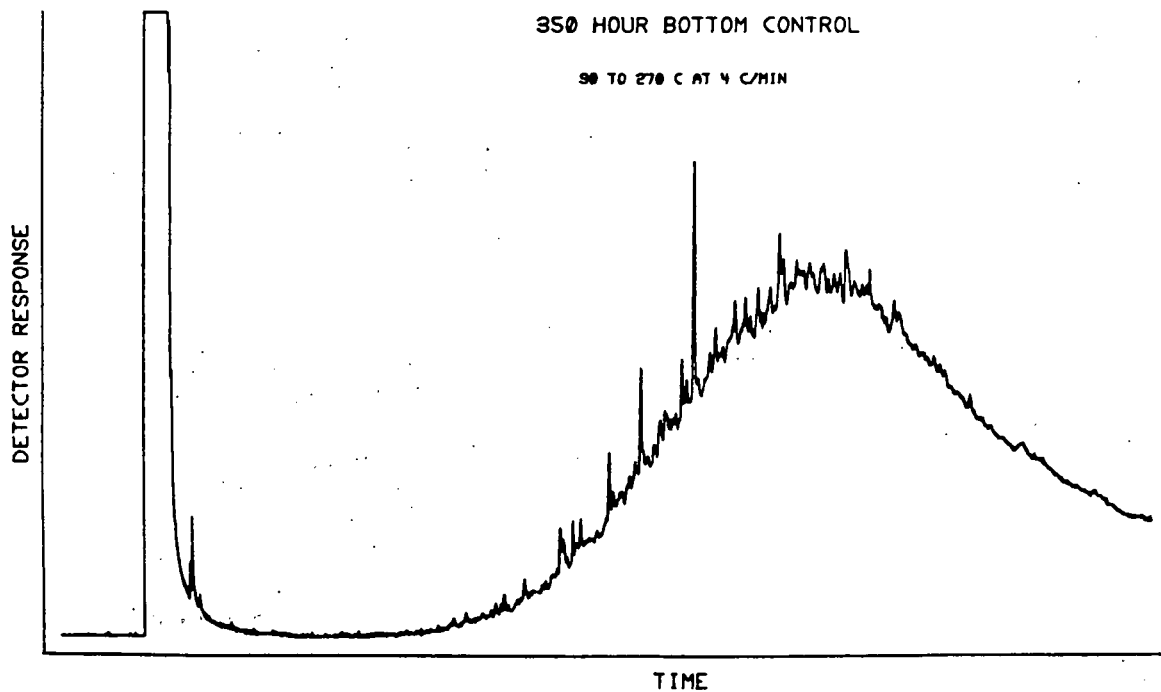


Figure 7.4.40 GC of Bottom Control after 350 hrs. (Trial 2)



peaks. This series of peaks is also observed in a number of the gas chromatograms from the oil contaminated tanks when petroleum hydrocarbons are not observed. These peaks appear to be due to chemicals of biological origin. The large quantitative values from the 350 hour middle and bottom samples are supported by the large unresolved envelope in the GC's of the two samples shown in Figures 7.4.29 and 7.4.40. The origin of the chemicals giving rise to their envelope are unknown; however, a similarly high quantitative value and unresolved envelope were observed for the sample from the bottom of the oil tank collected at 350 hours (Figure 7.4.56).

Oil Tank:

GC's of samples from the oil contaminated tank are shown in Figures 7.4.41-7.4.56. Prior to addition of the oil, the GC of a sample from the middle of the tank, Figure 7.4.41 is almost identical to that from the middle of the control tank (Figure 7.4.24). Samples from the oil tank at 1 and 24 hours do not show an appreciable increase in extractable organics over the control amounts and the GC's (Figures 7.4.32-7.4.34) are very similar to those of the control sample.

The GC of the sample from the oil tank taken from the top at 48 hours (Figure 7.4.35) shows a distribution of normal paraffins that are typical of petroleum and the quantitative value is over 1,000 ppb. The GC is interesting in that only the normal paraffins between C₁₄ and C₂₂ are observed. Moreover, the amounts of pristane and phytane relative to the normal paraffins are much larger than in the neat oil (see Figure 7.4.76).

The GC of the sample taken from the top (Figure 7.4.48) and bottom (Figure 7.4.50) at 72 hours also indicates a distribution of petroleum similar to that discussed above. It is interesting to note that the oil seems to be migrating to the bottom. At 192 hours, petroleum hydrocarbons appear in the GC (Figure 7.4.51) from the top of the tank, but they could not be discerned in the GC of the samples from the other two levels.

At 350 hours, GC of the samples (Figures 7.4.54-7.4.56) are very similar to those of the control tanks. As mentioned previously, the GC of the bottom sample has a large unresolved envelope. However, since samples from the control tank had a very similar GC, this large envelope is probably not due to petroleum.

Oil/Dispersant tank:

GC's of samples from the oil/dispersant tank are shown in Figures 7.4.57-7.4.75. Again, the GC of the sample from the middle of this tank prior to addition of the oil-dispersant is very similar to that of the control tank. GC's of the top and middle samples at 1 hour (Figures 7.4.58-7.4.59) and 24 hours (Figures 7.4.61-7.4.62) indicate a distribution of petroleum hydrocarbons very similar to the neat oil. It should be noted that the GC's of the samples from the top port contain more of the light components (C₁₀-C₁₂) than those from the middle port. Moreover, there is an increase in the amounts of pristane and phytane relative to the normal paraffins between the 1 and 24 hour samples.

Figure 7.4.41 GC of Middle Oil at 0 hr. (Contaminated Tank)

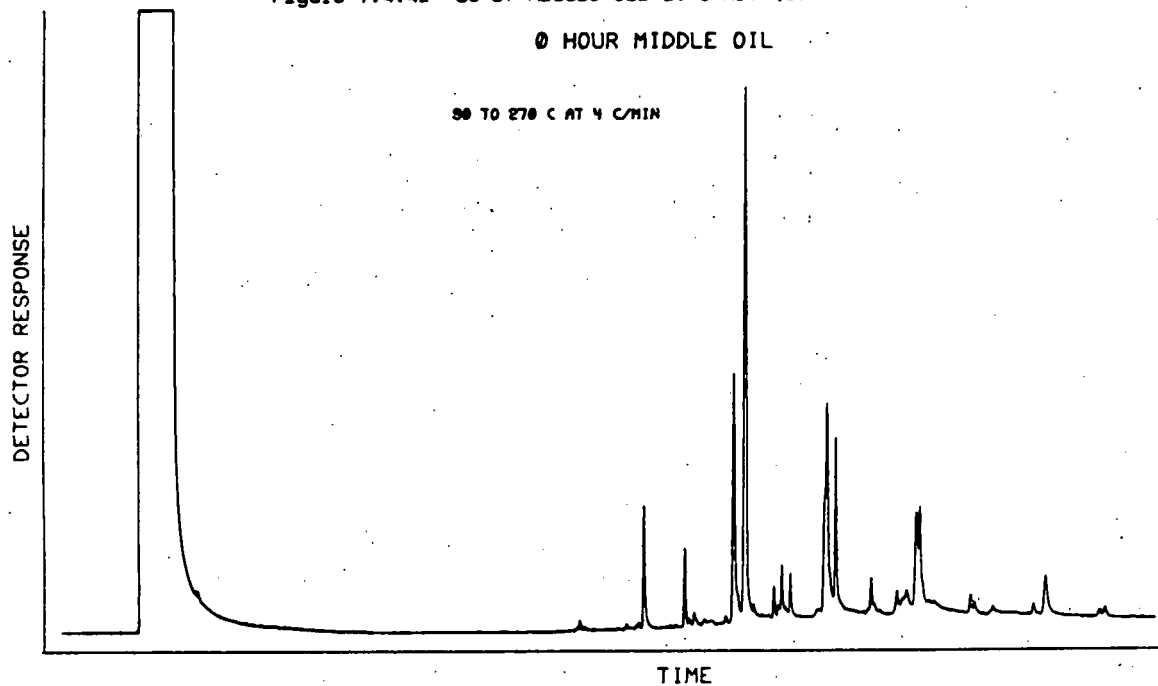


Figure 7.4.42 GC of Middle Oil after 1 hr.

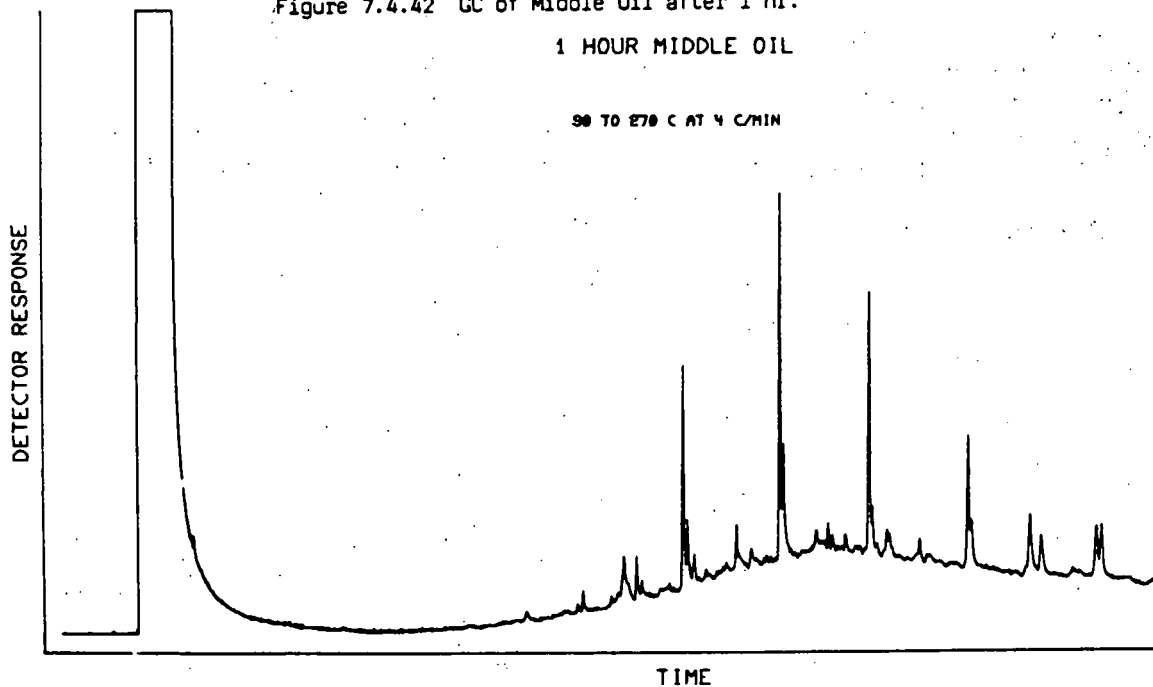


Figure 7.4.43 GC of Top Oil after 24 hrs.

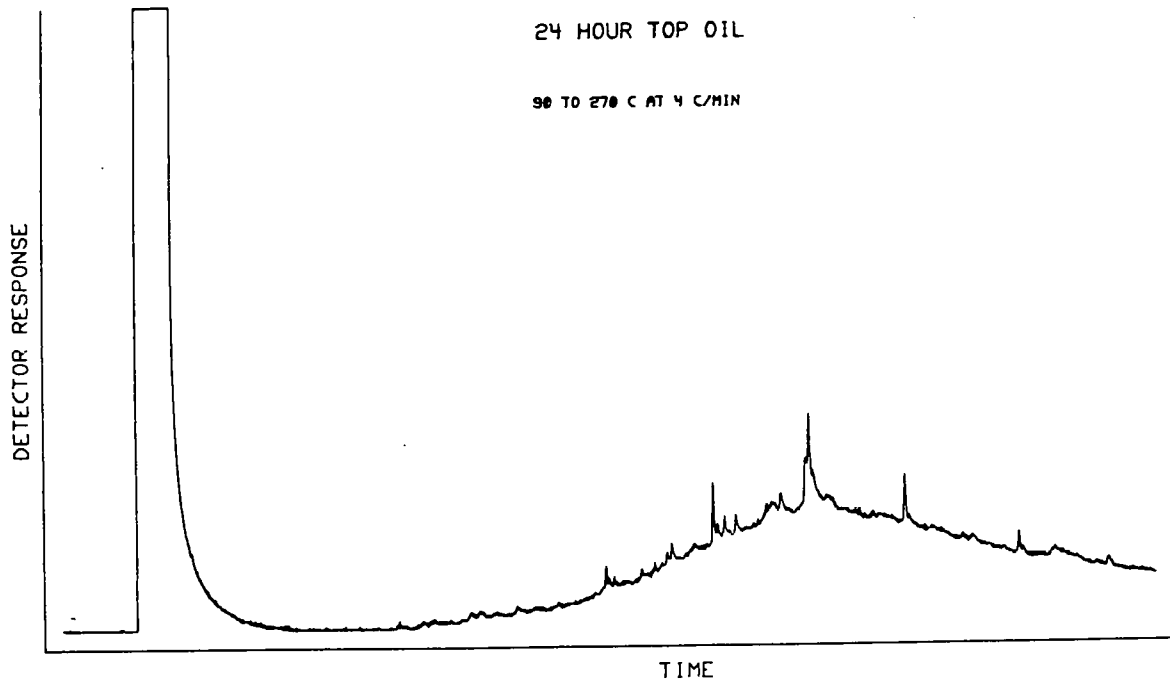


Figure 7.4.44 GC of Middle Oil after 24 hrs.

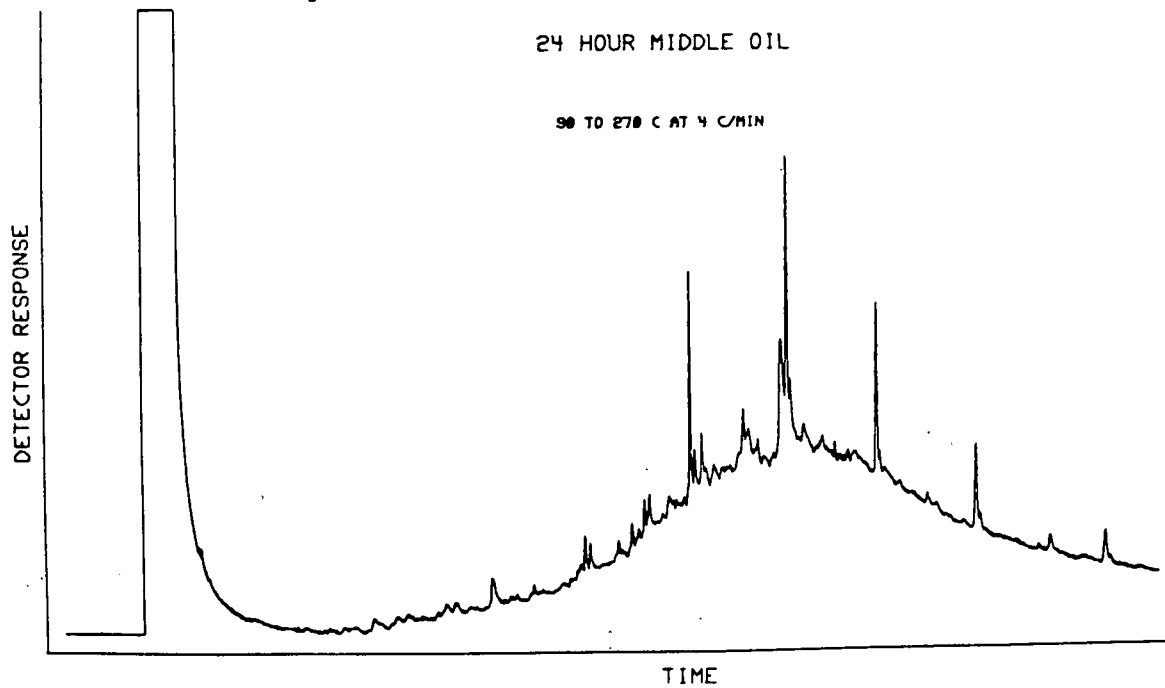


Figure 7.4.45 GC of Top Oil after 48 hrs.

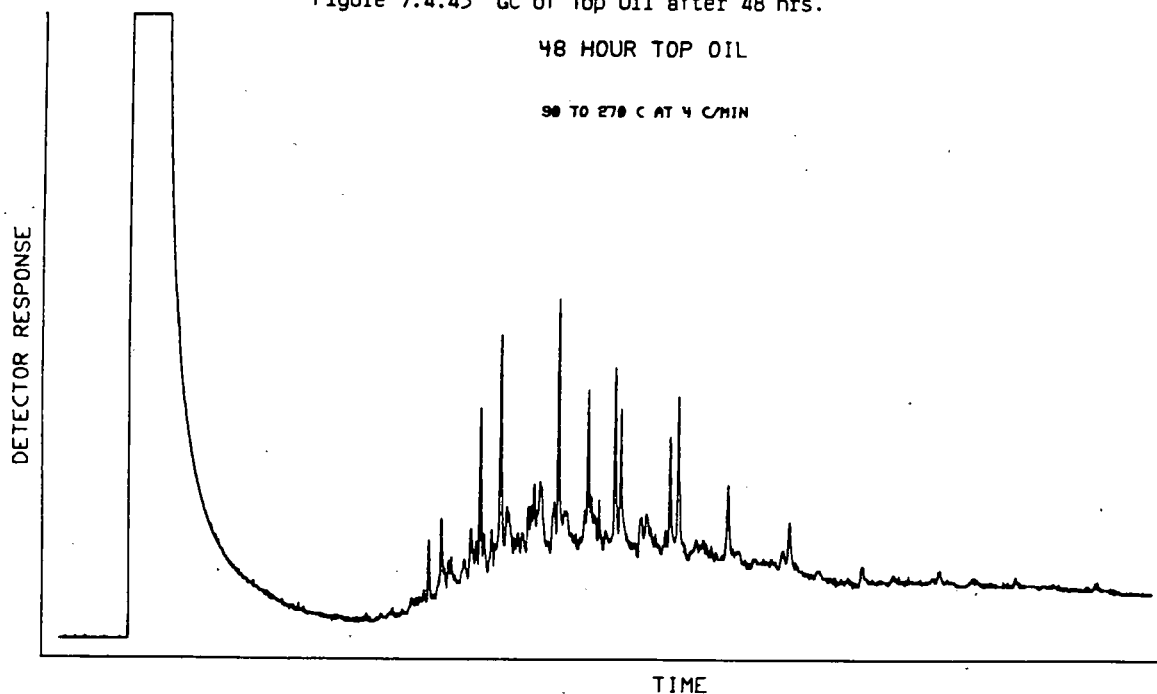


Figure 7.4.46 GC of Middle Oil after 48 hrs.

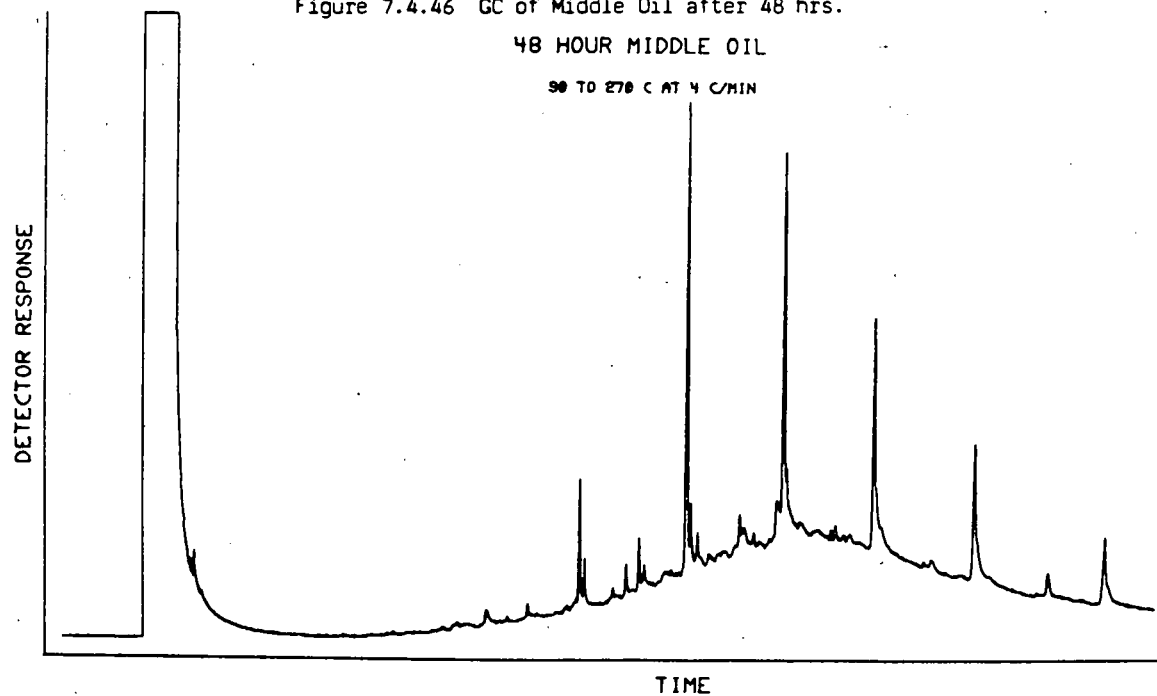


Figure 7.4.47 GC of Bottom Oil after 48 hrs.

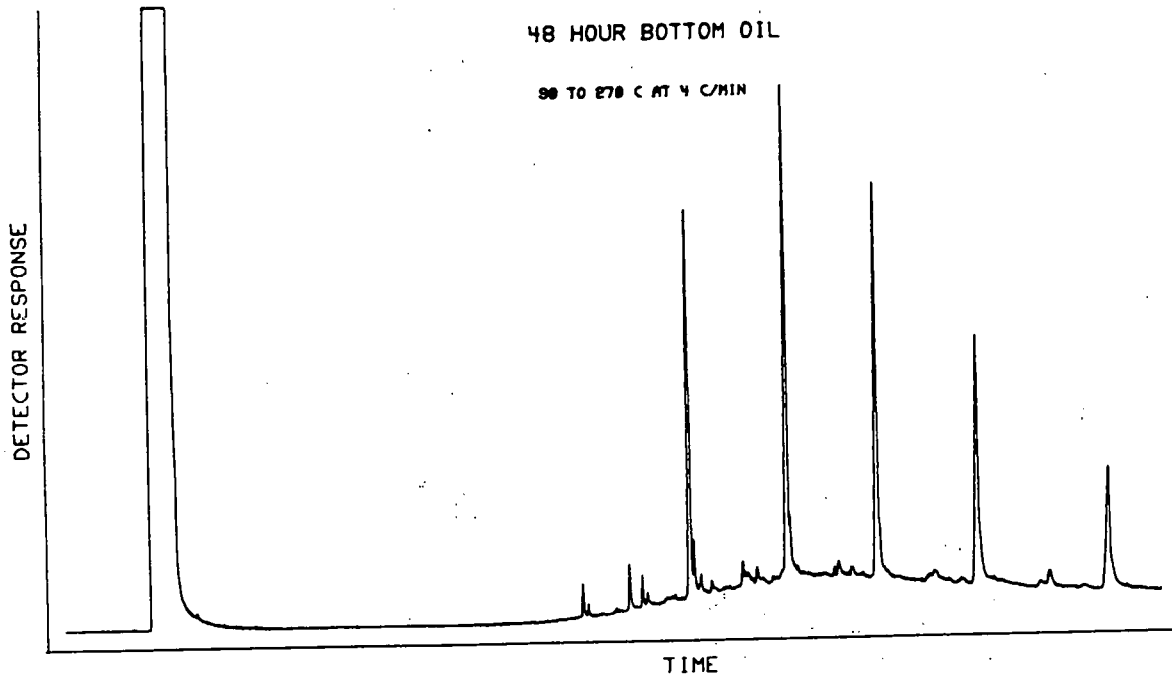


Figure 7.4.48 GC of Top Oil after 72 hrs.

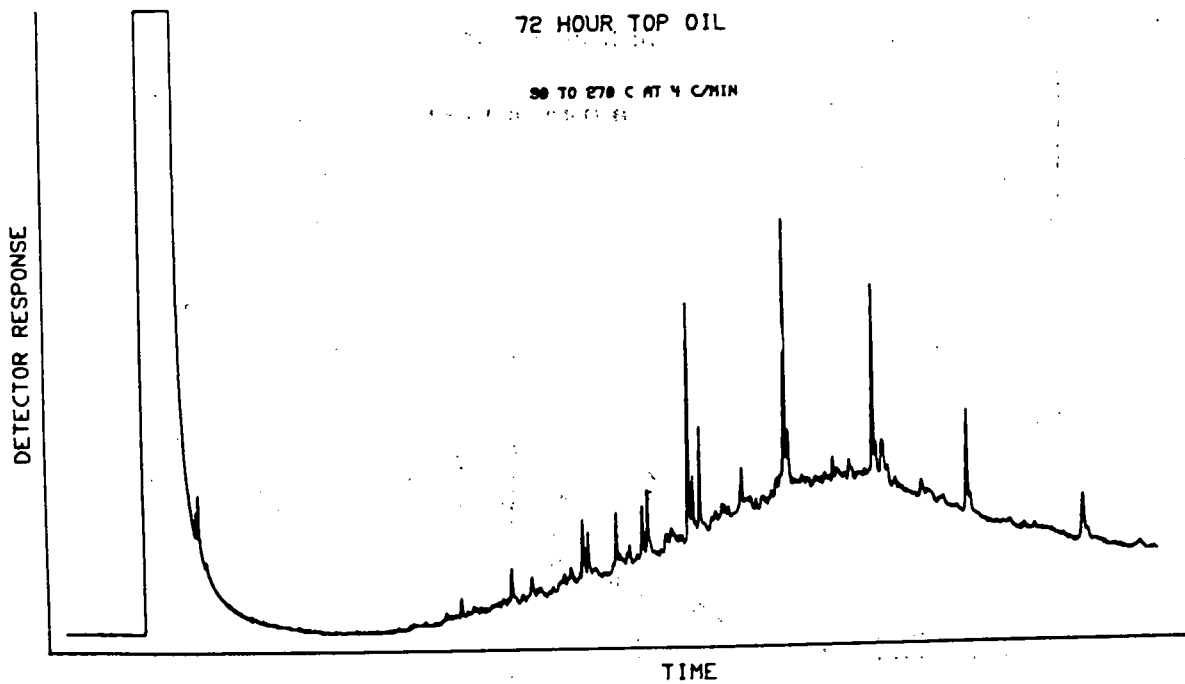


Figure 7.4.49 GC of Middle Oil after 72 hrs. (Contaminated Tank)

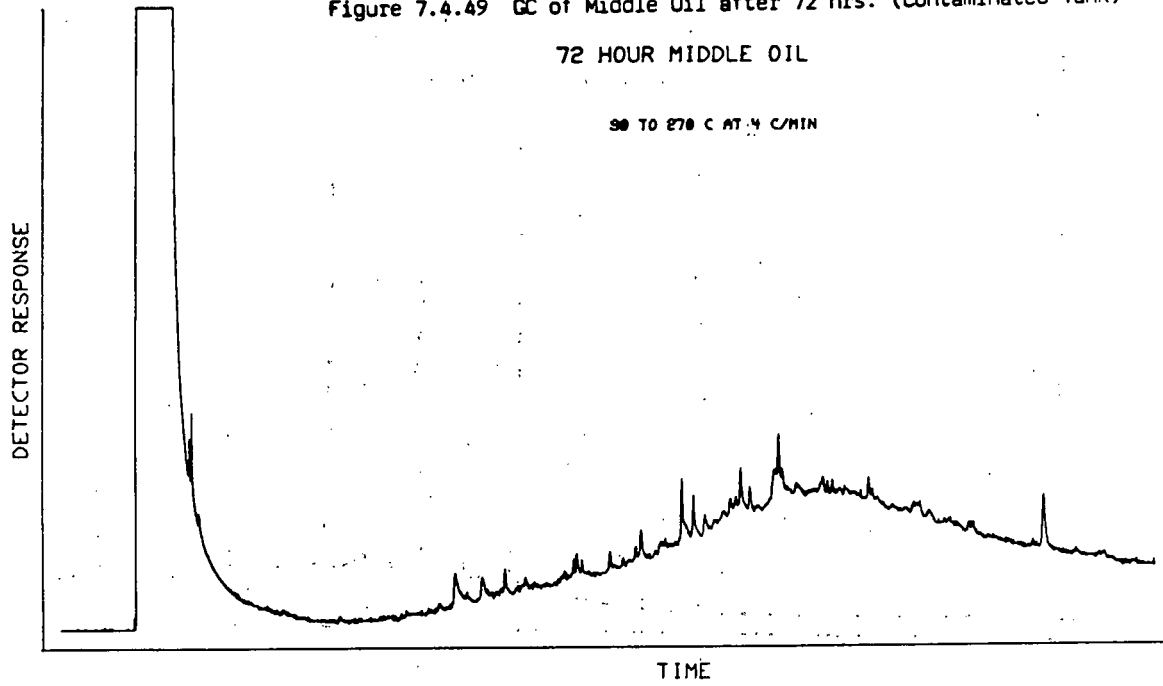


Figure 7.4.50 GC of Bottom Oil after 72 hrs.

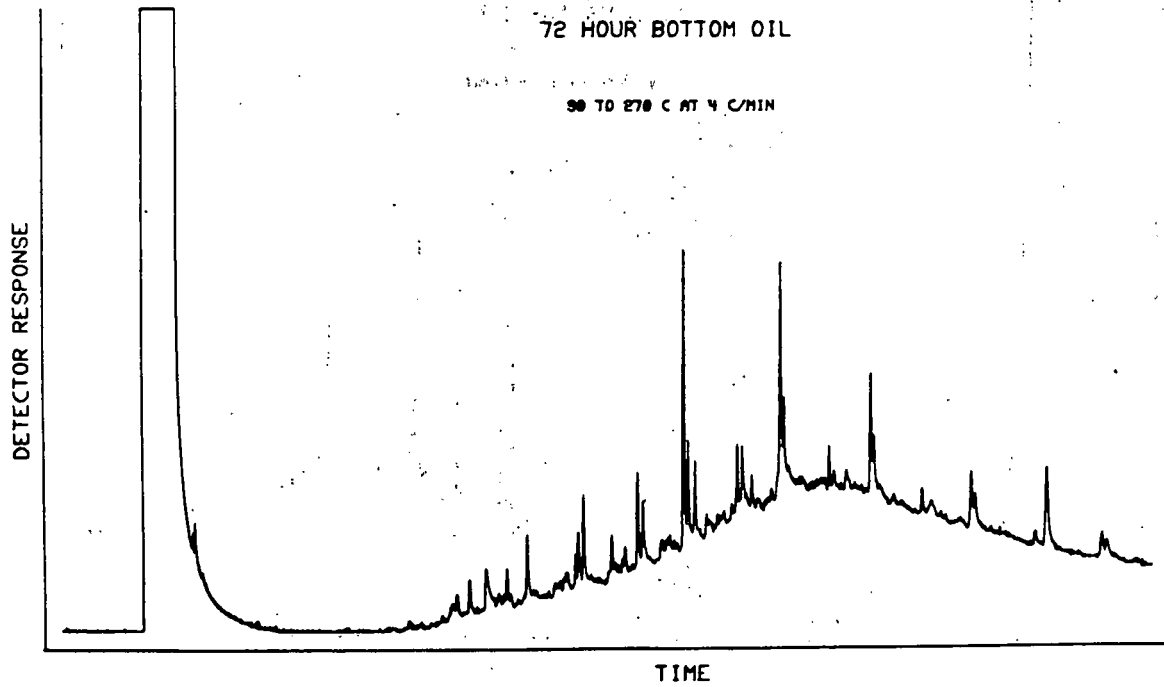


Figure 7.4.51 GC of Top Oil after 192 hrs.

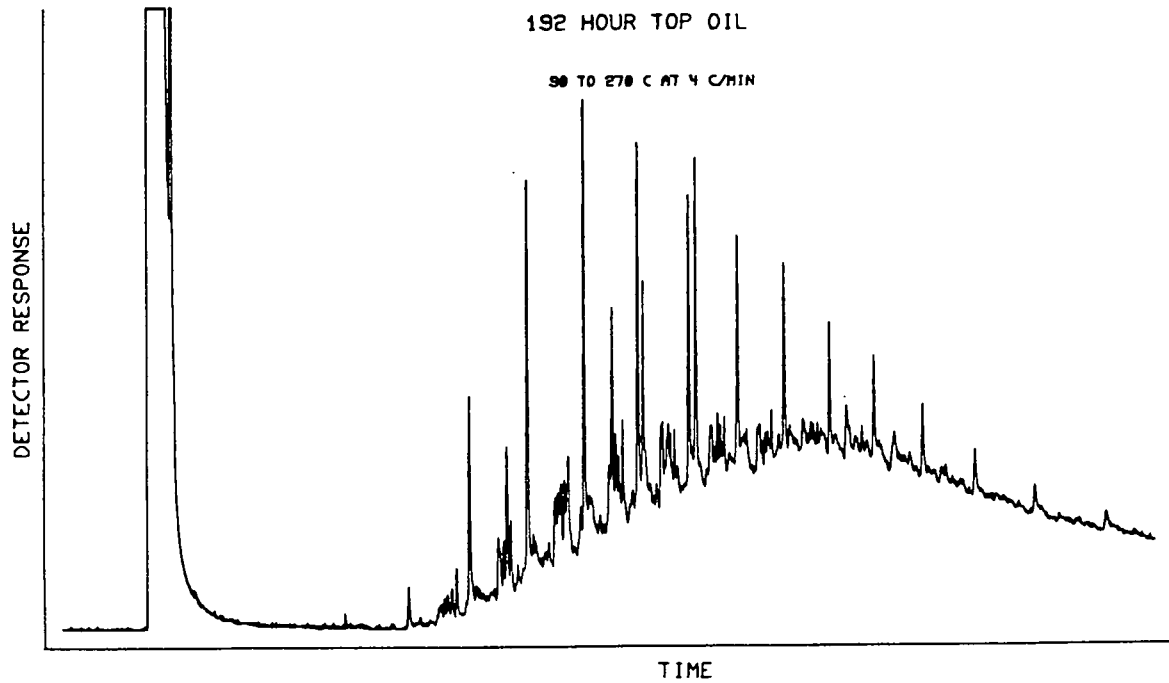


Figure 7.4.52 GC of Middle Oil after 192 hrs.

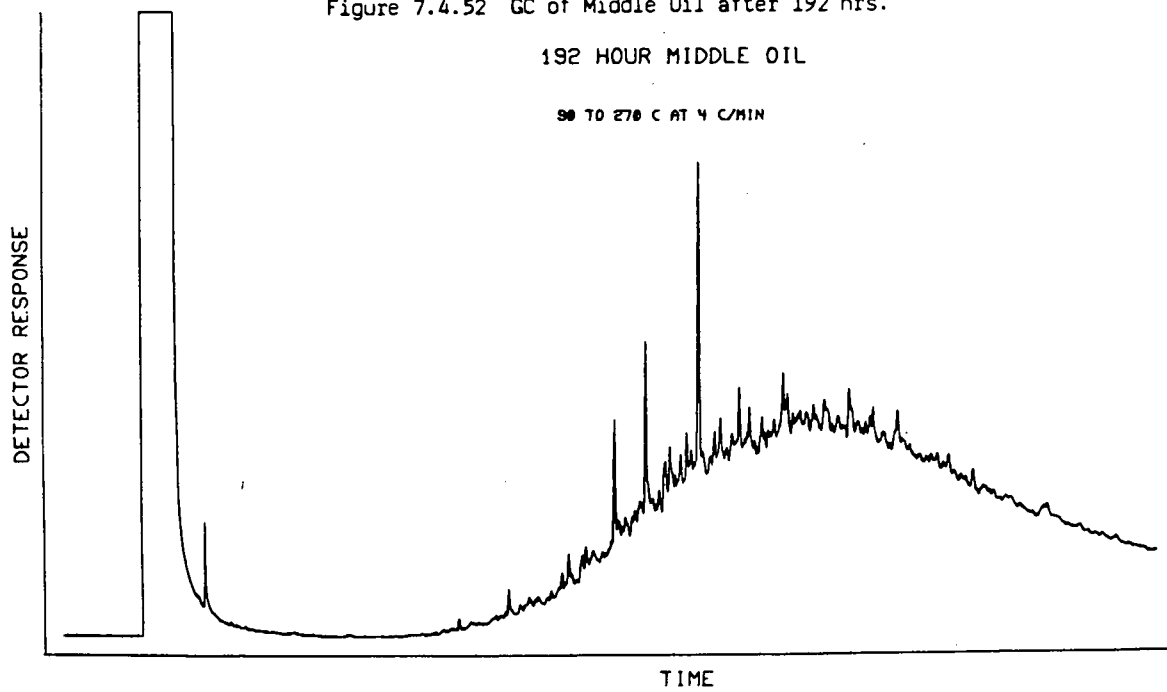


Figure 7.5.53 GC of Bottom Oil after 192 hrs.

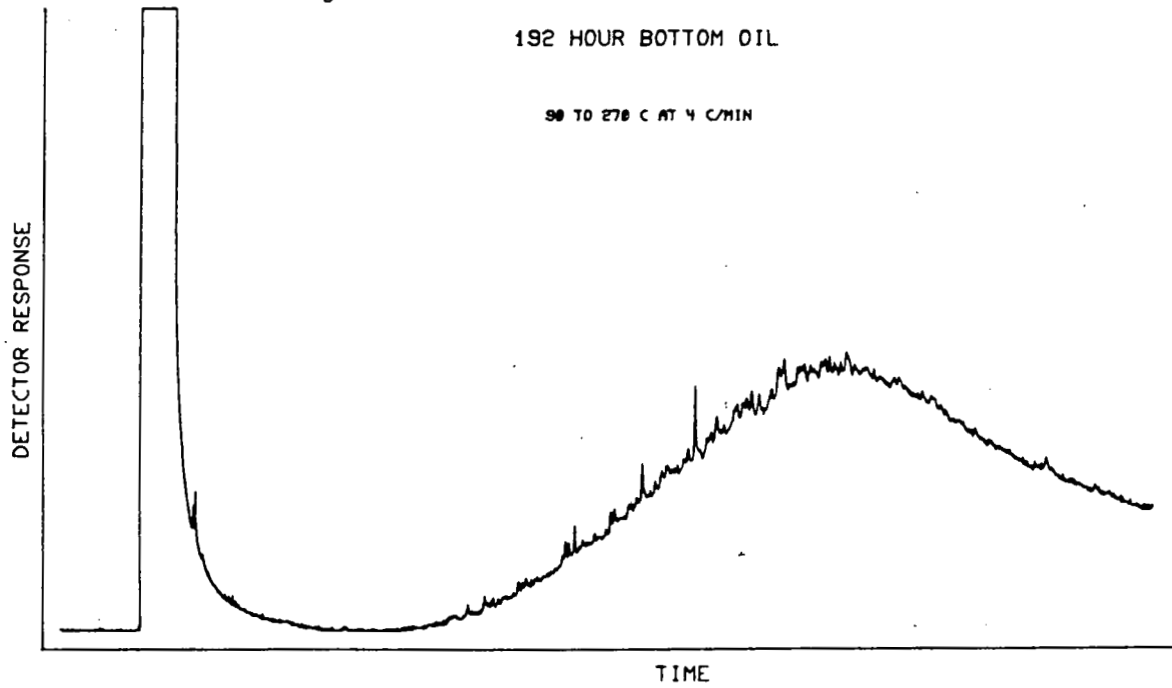


Figure 7.4.54 GC of Top Oil after 350 hrs.

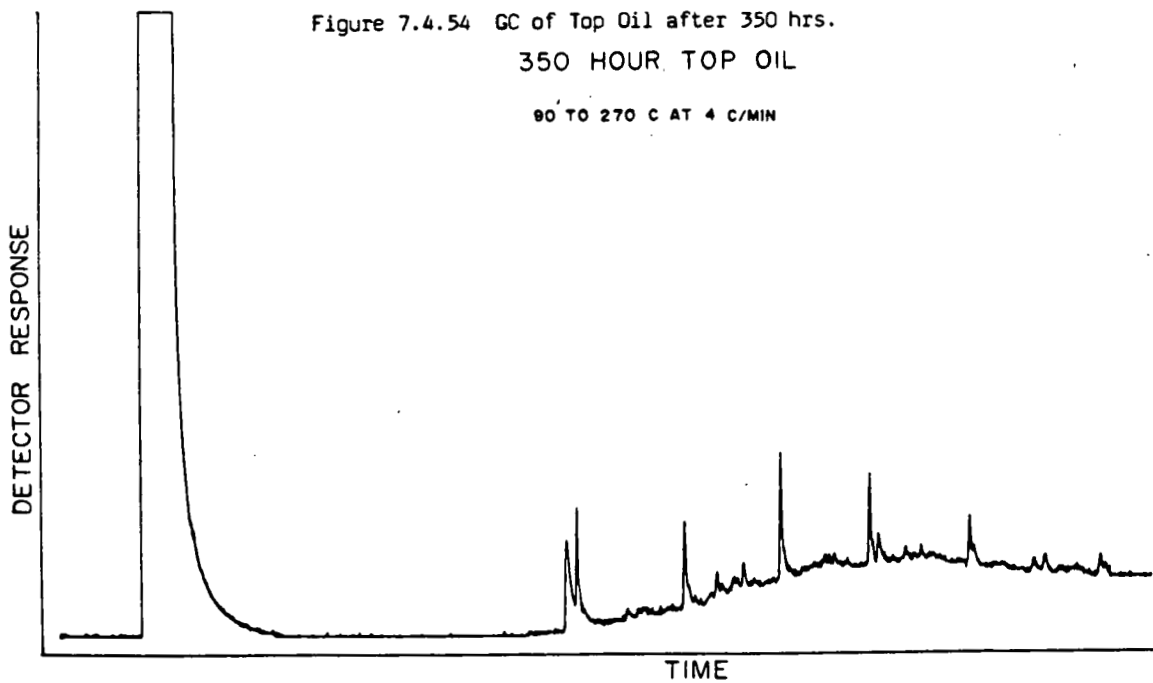


Figure 7.4.55 GC of Middle Oil after 350 hrs.

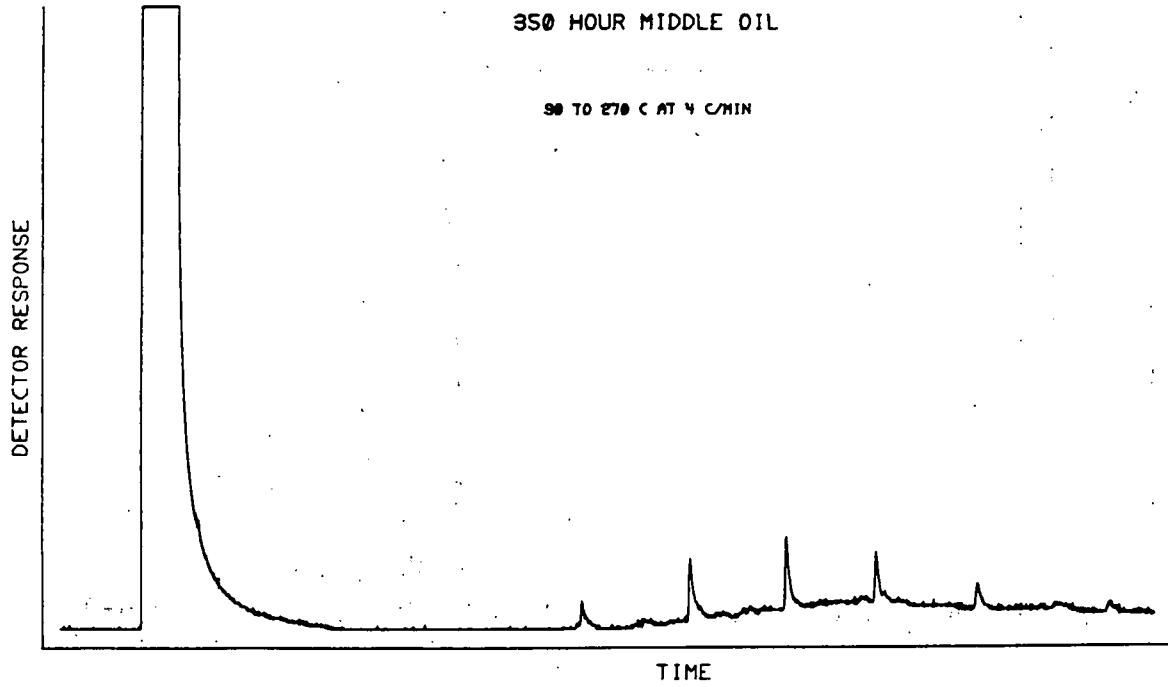


Figure 7.4.56 GC of Bottom Oil after 350 hrs.

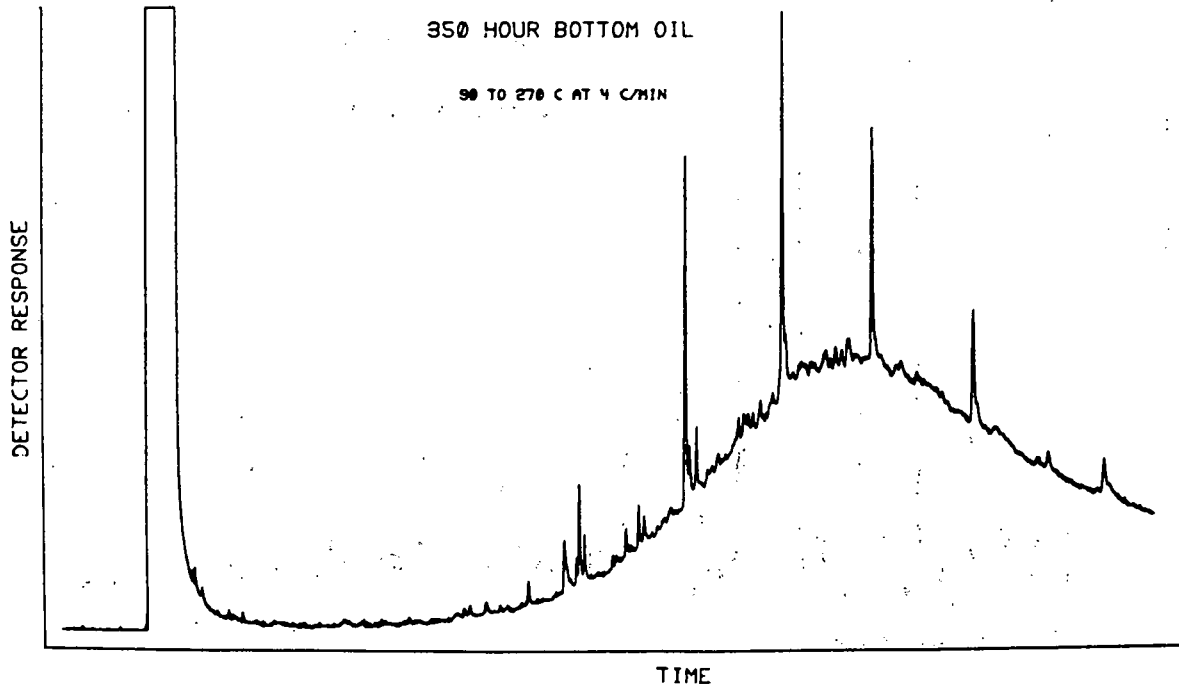


Figure 7.4.57 GC of Middle of Oil/Dispersant Tank at 0 hrs.

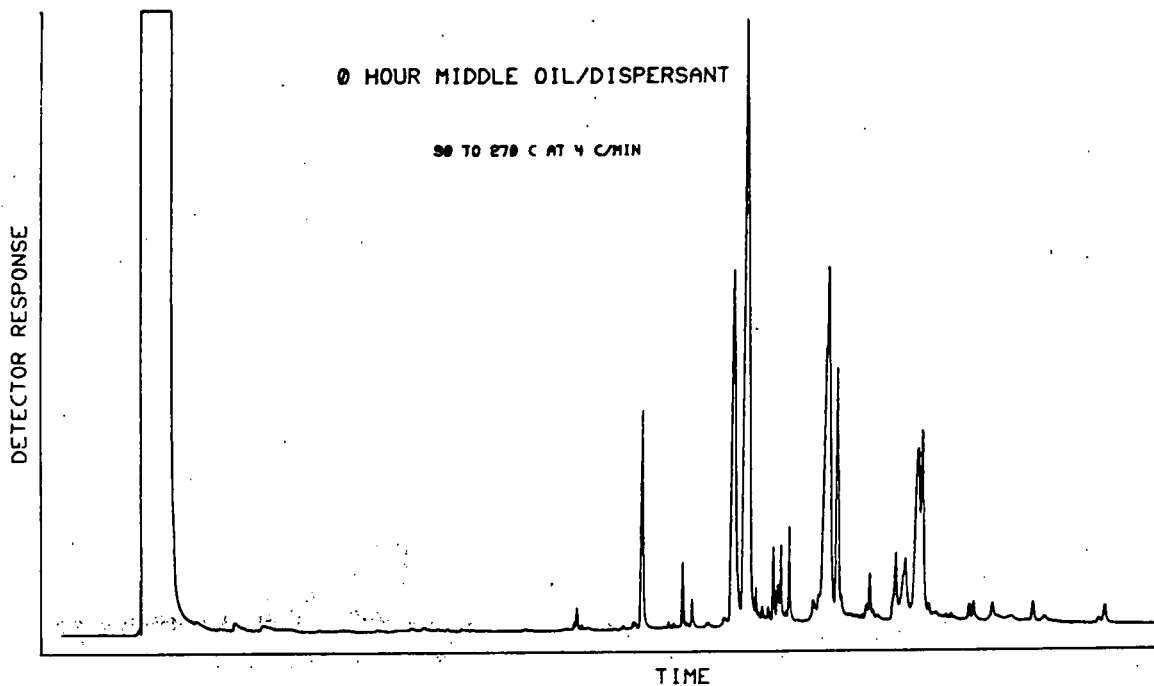


Figure 7.4.58 GC of Top of Oil/Dispersant Tank at 1 hr.

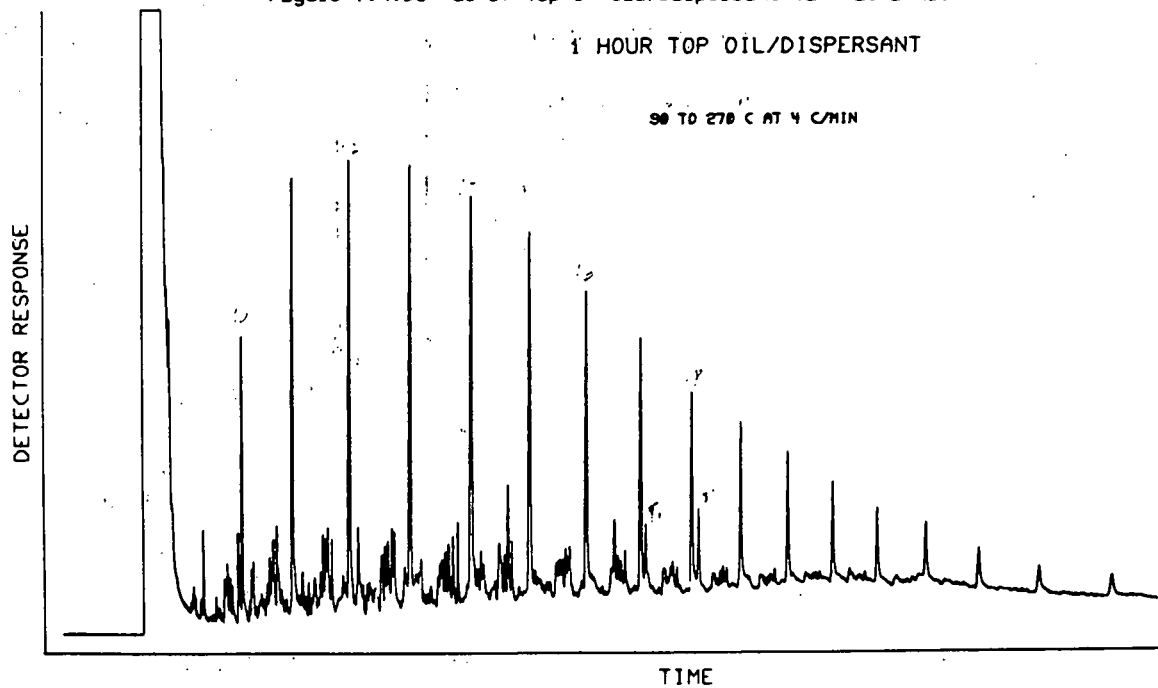


Figure 7.4.59 GC of Middle of Oil/Dispersant Tank at 1 hr.

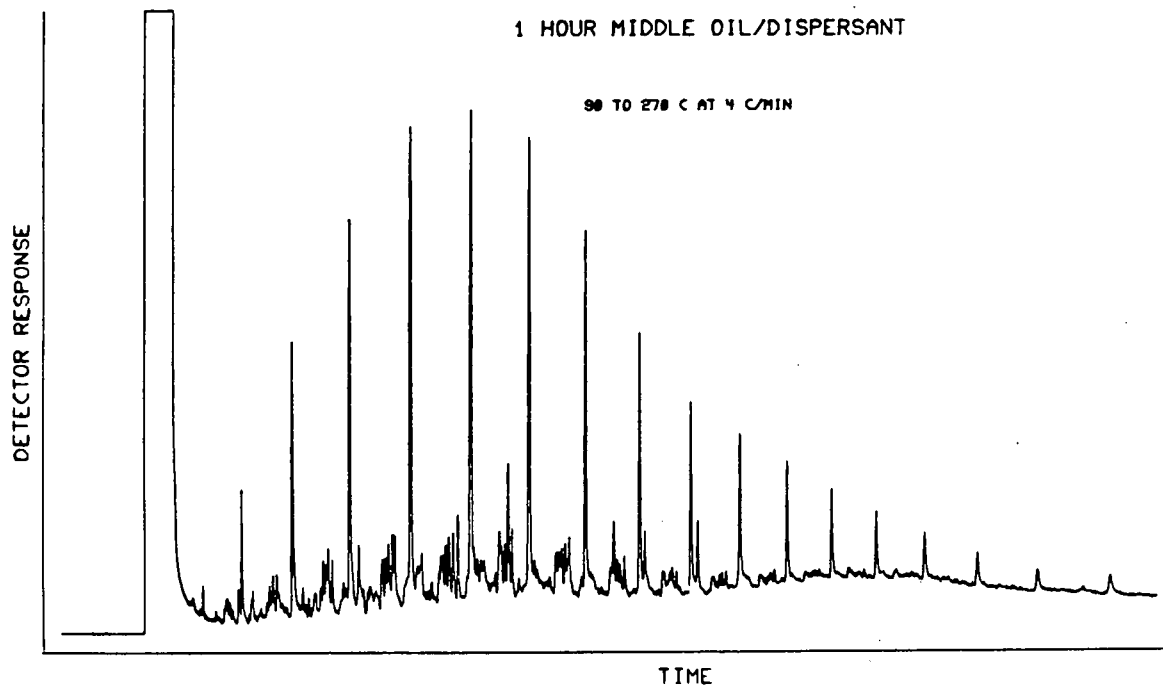


Figure 7.4.60 GC of Bottom of Oil/Dispersant Tank at 1 hr.

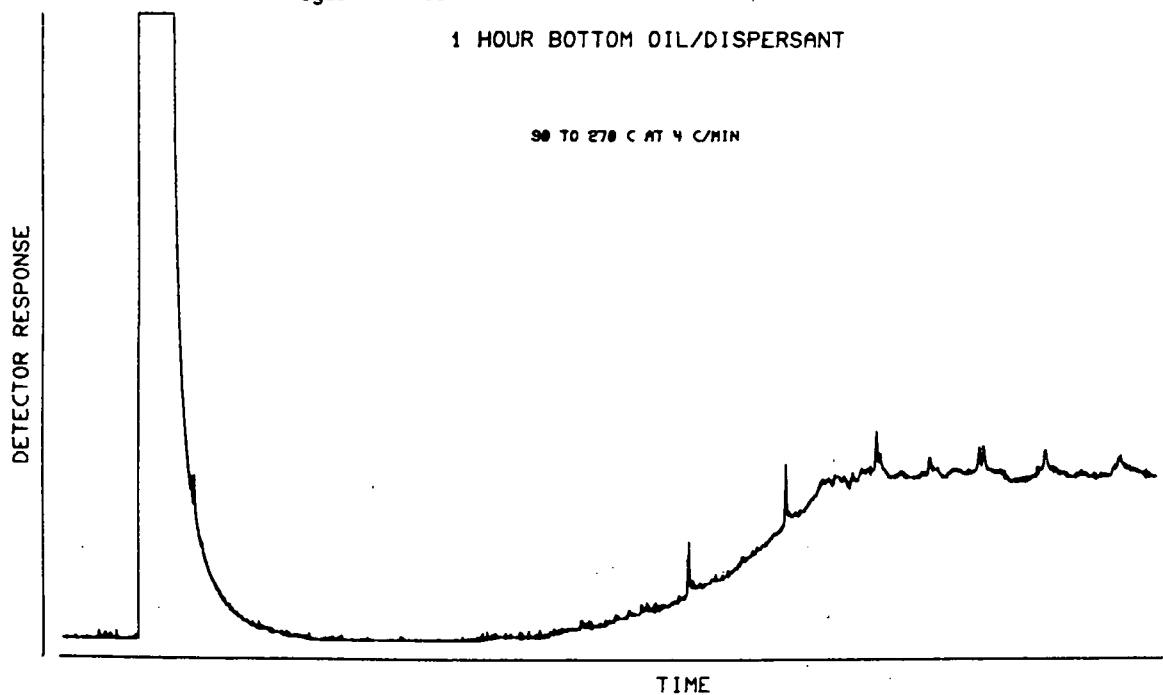


Figure 7.4.61 GC of Top of Oil/Dispersant Tank at 24 hrs.

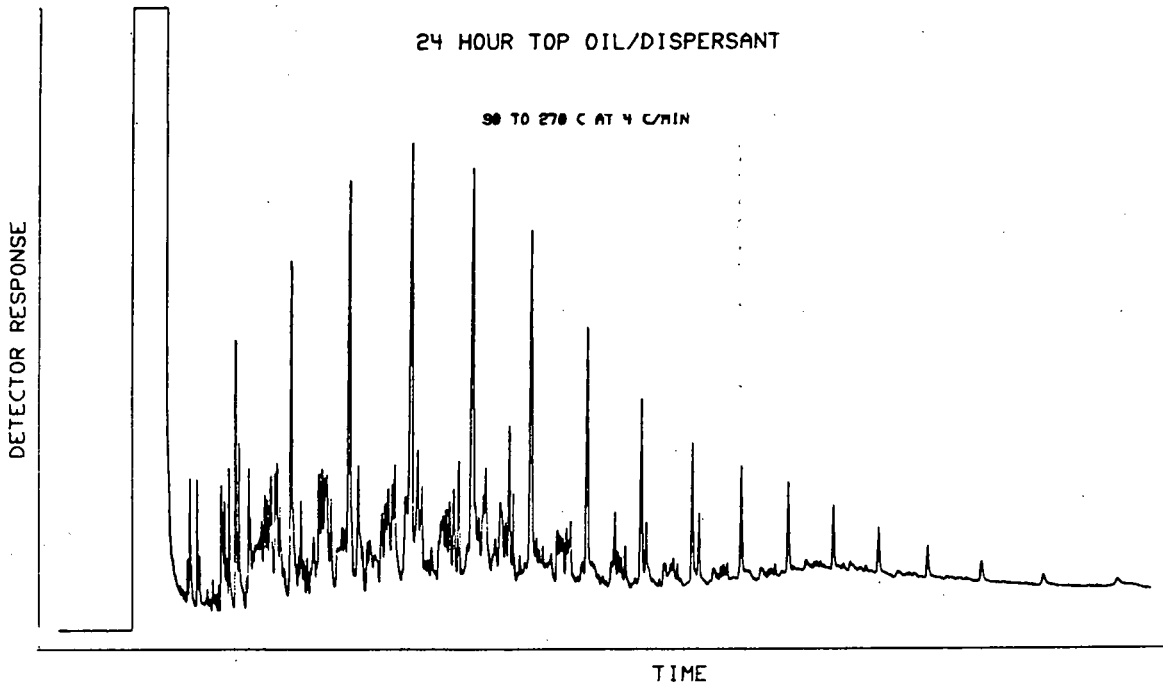


Figure 7.4.62 GC of Middle of Oil/Dispersant Tank at 24 hrs.

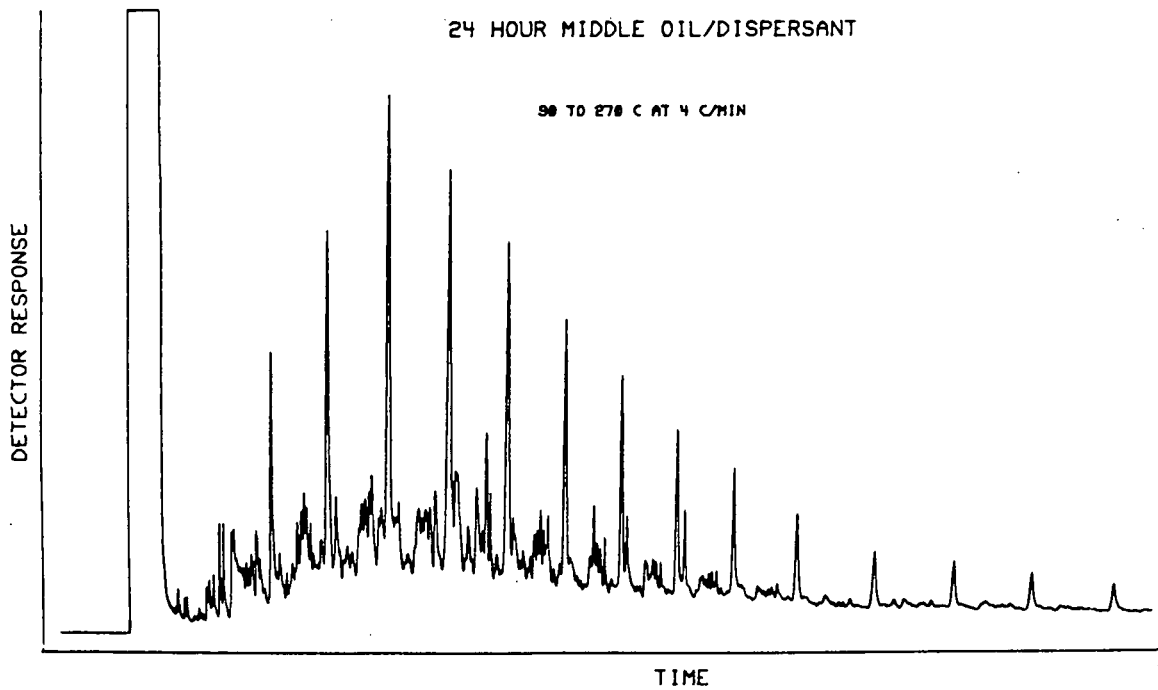


Figure 7.4.63 GC of Bottom of Oil/Dispersant Tank at 24 hrs.

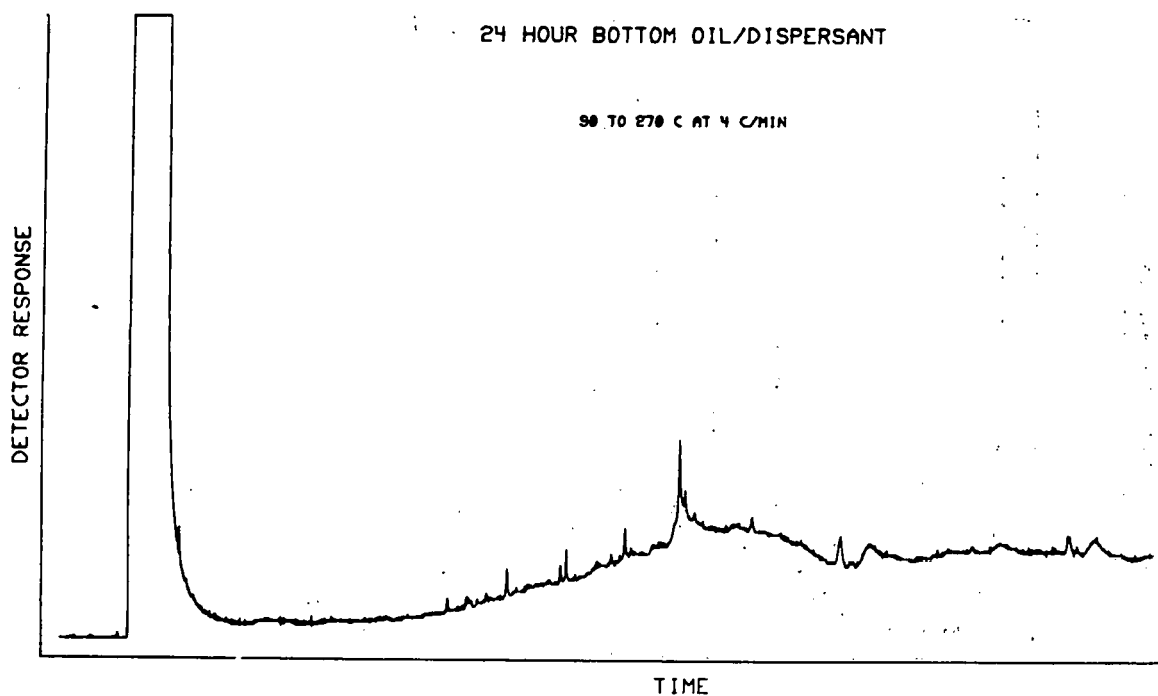


Figure 7.4.64 GC of Top of Oil/Dispersant Tank at 48 hrs.

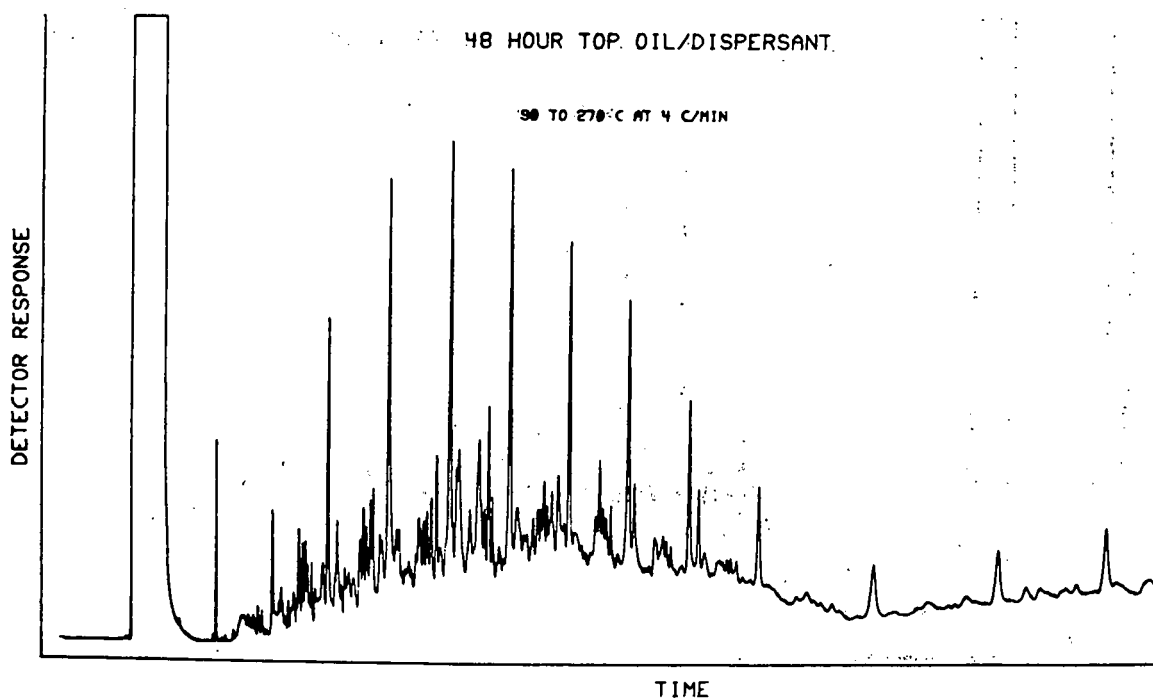


Figure 7.4.65 GC of Middle of Oil/Dispersant Tank at 48 hrs.

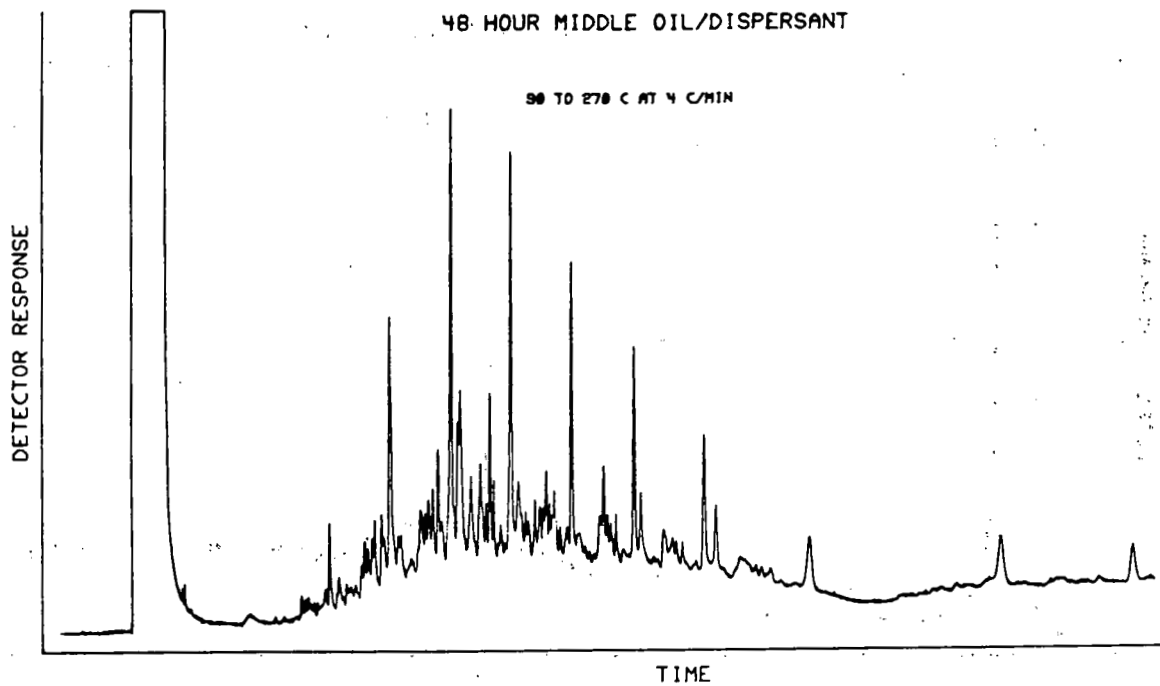


Figure 7.4.66 GC of Bottom of Oil/Dispersant Tank at 48 hrs.

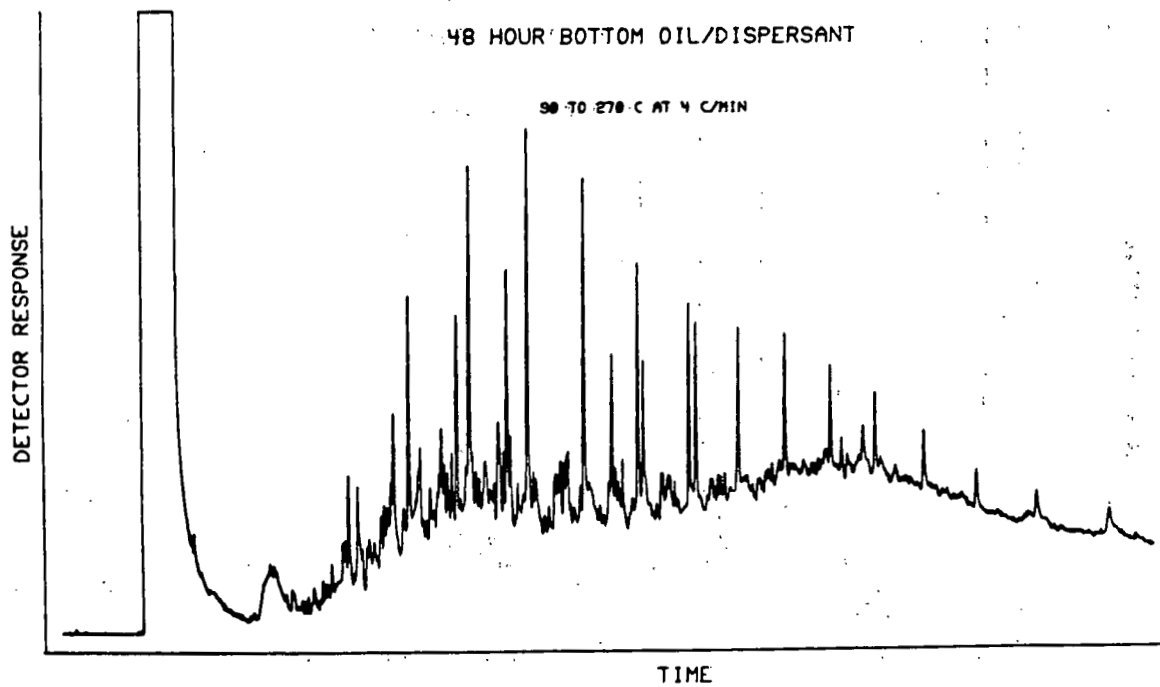


Figure 7.4.67 GC of Top of Oil/Dispersant Tank at 72 hrs.

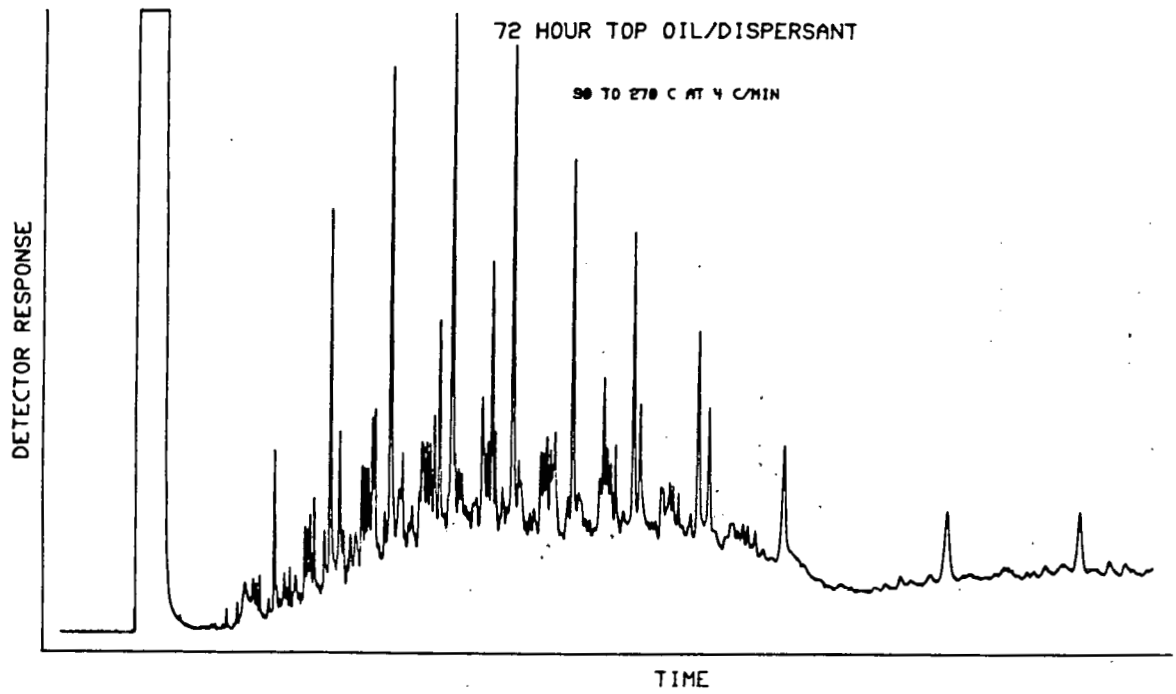


Figure 7.4.68 GC of Middle of Oil/Dispersant Tank at 72 hrs.

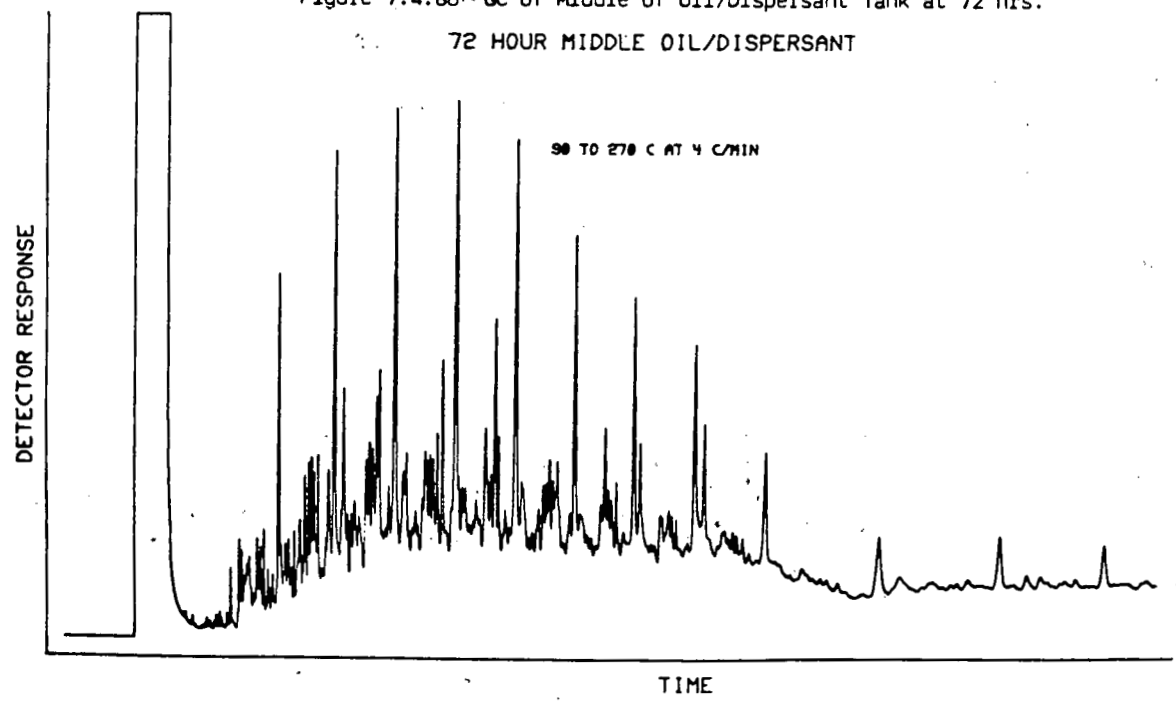


Figure 7.4.69 GC of Bottom of Oil/Dispersant Tank at 72 hrs.

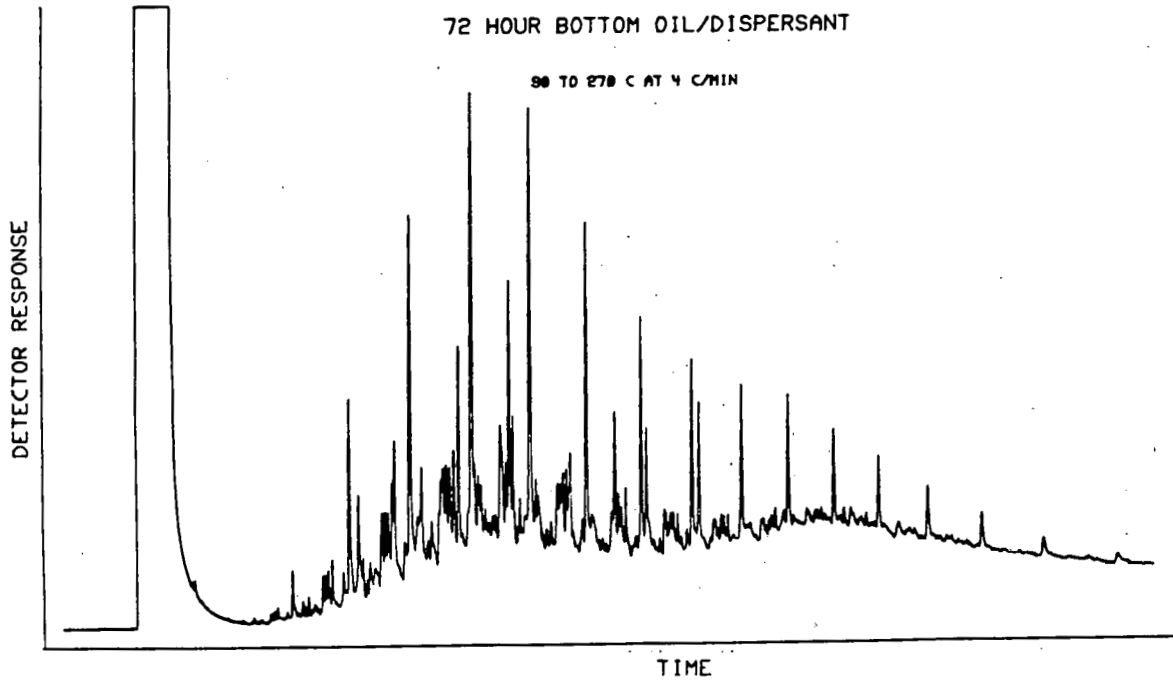
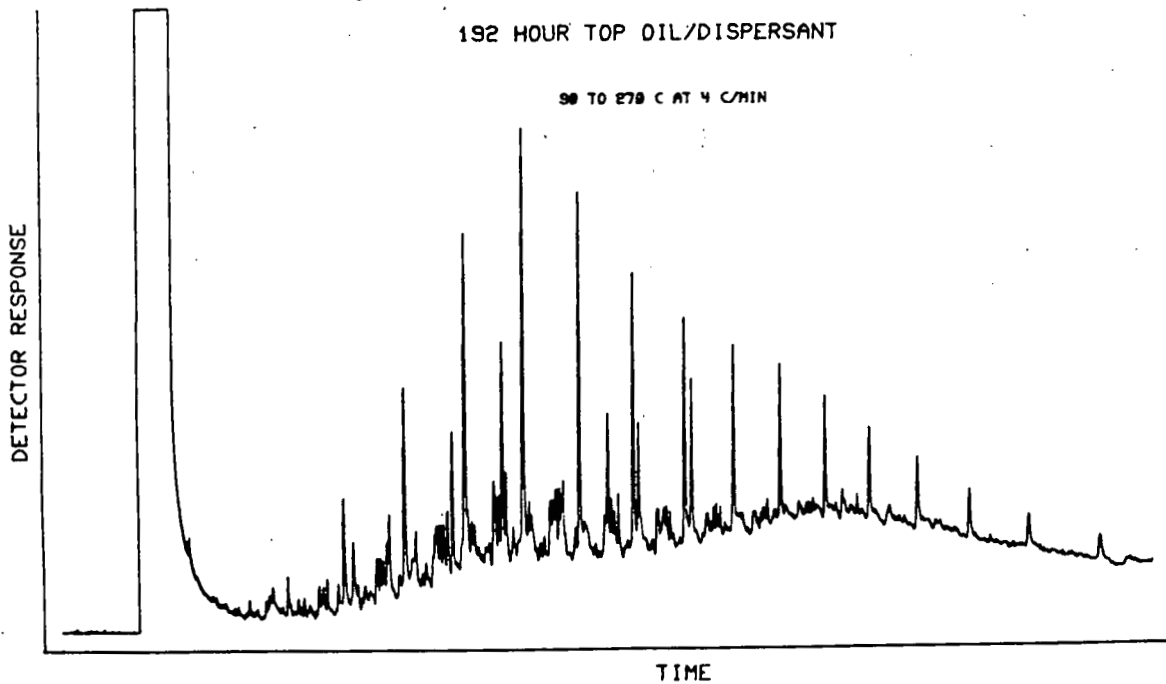


Figure 7.4.70 GC of Top of Oil/Dispersant Tank at 192 hrs.



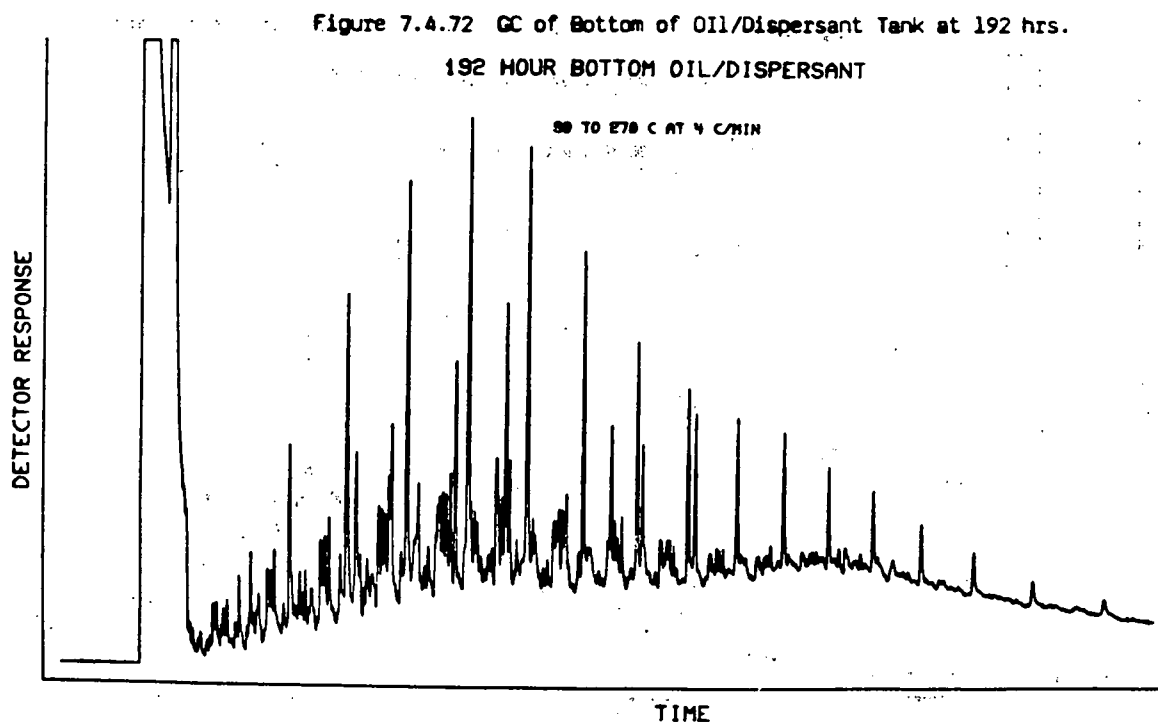
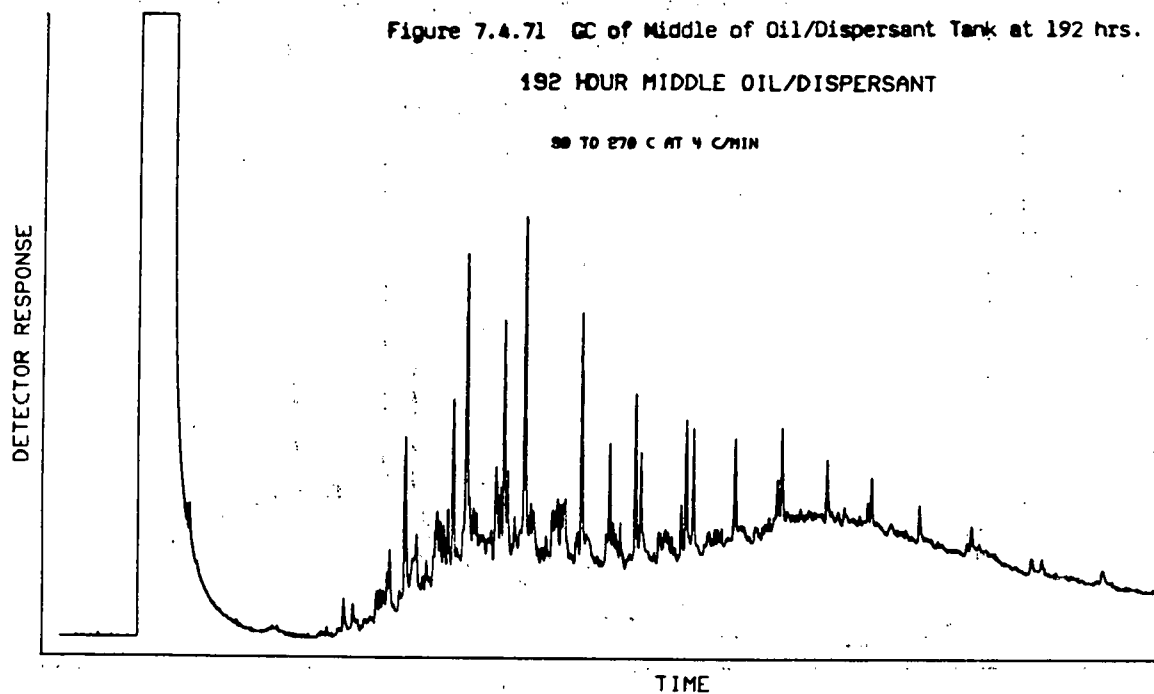


Figure 7.4.73 GC of Top of Oil/Dispersant Tank at 350 hrs.

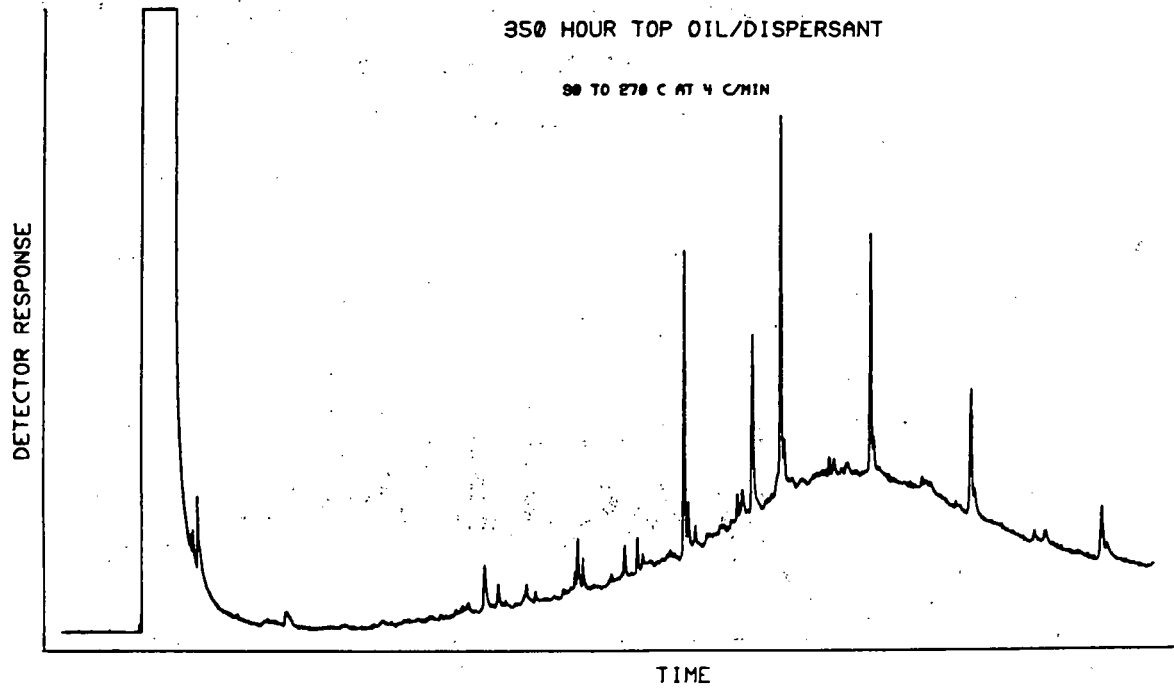
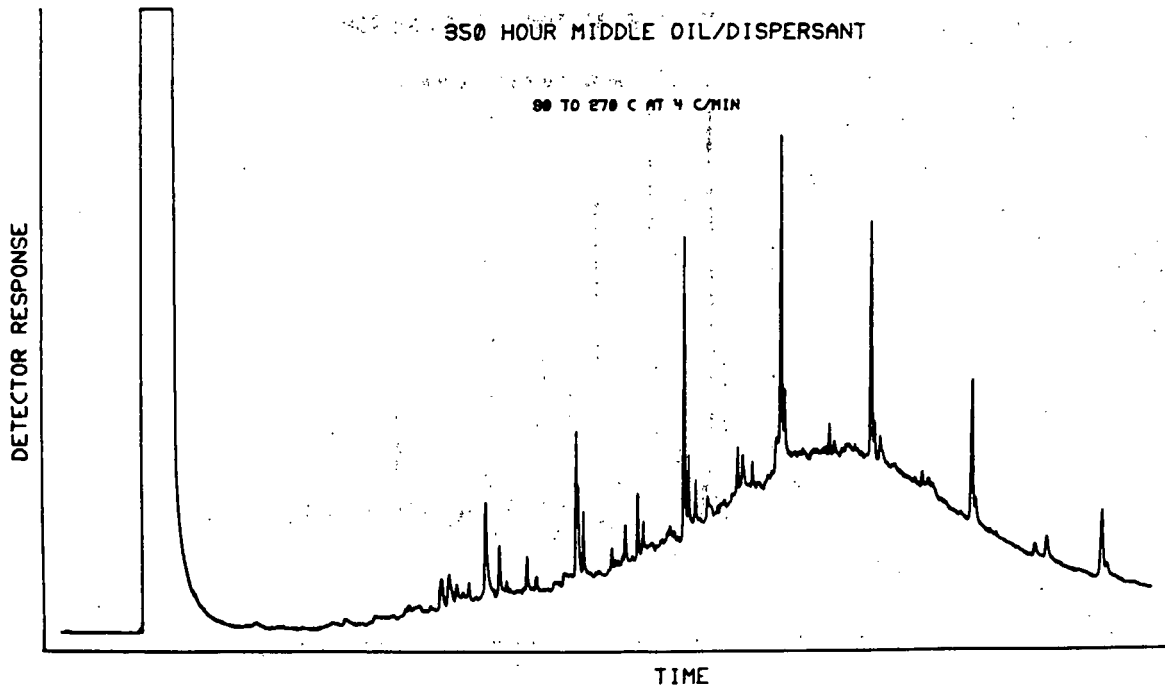


Figure 7.4.74 GC of Middle of Oil/Dispersant Tank at 350 hrs.



At 48 hours, petroleum hydrocarbons are observed in the GC's (Figures 7.4.64-7.4.66) of samples from all three ports. The relative amounts of light hydrocarbons decreases from the top to the bottom of the tank. Furthermore, the GC of the sample from the bottom of the tank shows a dramatic increase in the amounts of pristane and phytane relative to the normal paraffins. Moreover, there appears to be only one broad unresolved envelope centered at about the retention time of n-C₁₅ for the samples from the top and middle ports, whereas there is a second maximum centered at about n-C₂₂ in the GC of the sample from the bottom.

The GC of samples collected at 72 hours (Figure 7.4.67-7.4.69) are very similar to those at 48 hours; however, there is an increase in the amounts of pristane and phytane relative to the normal paraffins in the GC of the samples from the top and middle ports.

At 192 hours the GC's of samples from the three ports (Figures 7.4.70-7.4.72) are very similar, and only subtle differences can be detected. All three GC's appear to have a double unresolved envelope, with maxima at n-C₁₅ and n-C₂₁. The GC of the sample from the bottom port has a slightly greater amount of the lighter paraffins with a maximum of normal paraffins at n-C₁₄ rather than at n-C₁₅ as observed in the other two samples.

After 350 hours, the GC's of samples from the three ports have changed dramatically. The amounts of petroleum hydrocarbons relative to peaks found in the GC of control samples is very low in samples from the top two ports and it is difficult to identify them; the concentrations of samples from these two levels are at the control level. However, the sample from the bottom port still contains significant amounts of petroleum hydrocarbons as indicated in the GC shown in Figure 7.4.75. Again, the double unresolved envelope and the relatively high concentration of pristane and phytane are observed.

Fractionation of Samples

Extracts of water samples were separated into three fractions consisting of paraffins, aromatics and polar compounds. A GC of each fraction was measured. The GC of the neat oil is shown in Figure 7.4.76 and of the three fractions of the neat oil in Figure 7.4.77-7.4.79. The GC of the first two fractions contain a number of specific peaks, whereas the GC of the third fraction contains very few characteristic peaks.

GC's obtained by fractionating selected samples from the oil/dispersant tank collected at 24, 48 and 72 hours are shown in Figures 7.4.80 - 7.4.94. At 24 hours the paraffin fraction (Figure 7.4.80) from the top port is very similar to the paraffin fraction of the neat oil (Figure 7.4.77) except for the loss of the more volatile components from n-C₁₁ to n-C₁₄. The aromatic fraction (Figure 7.4.81 and 7.4.78) are also similar except for the loss of the lighter fractions. However, the GC of the polar fraction from the oil/dispersant tank (Figure 7.4.82) has no distinctive peaks suggesting that the polars are lost in the flow system.

Figure 7.4.75 GC of Bottom of Oil/Dispersant Tank at 350 hrs.

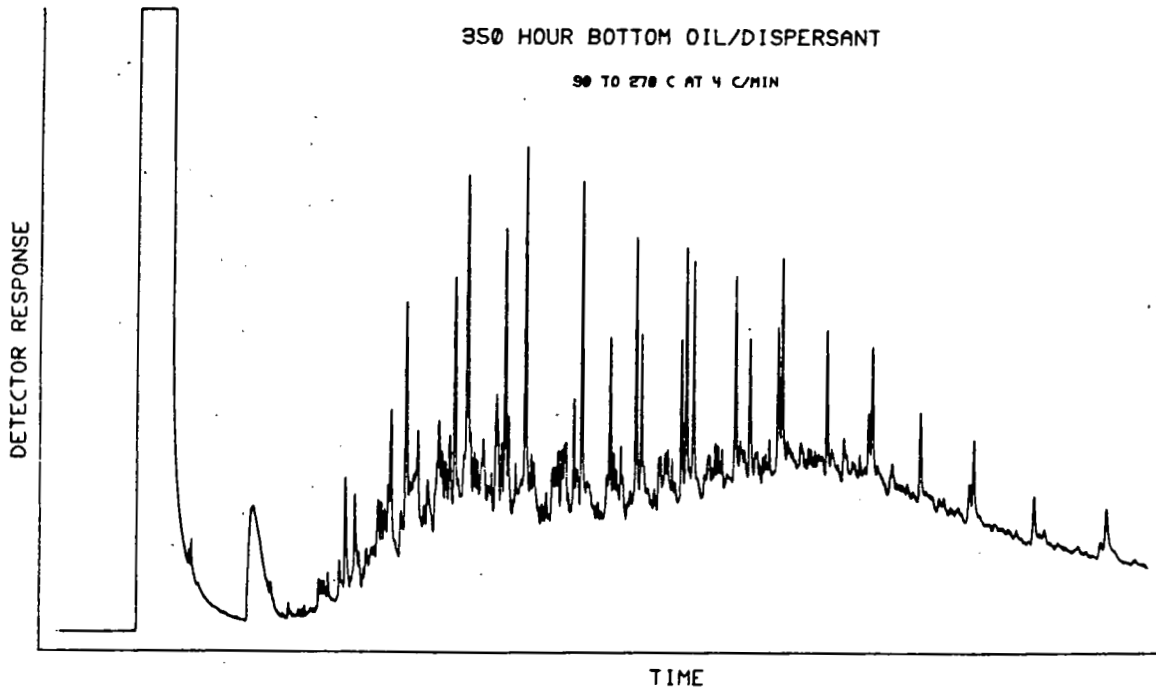


Figure 7.4.76 GC of Neat Oil

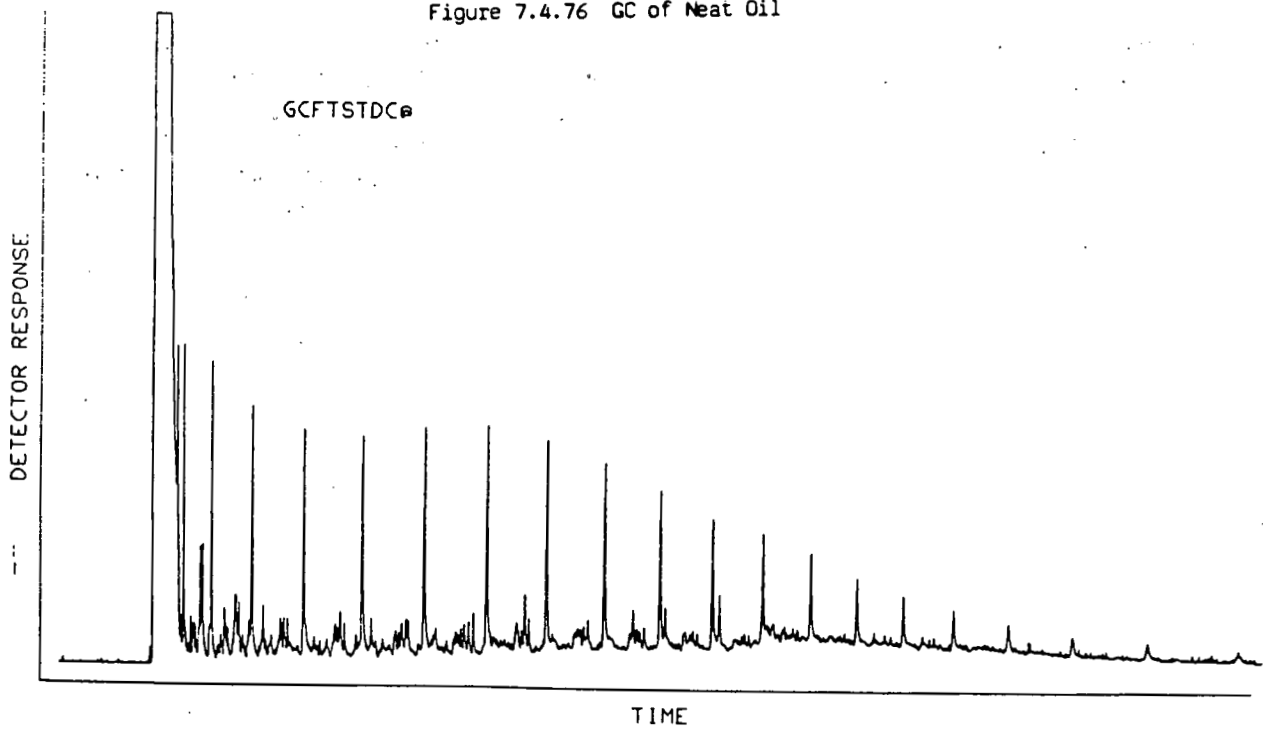


Figure 7.4.77 GC of Paraffin Fraction of Neat Oil

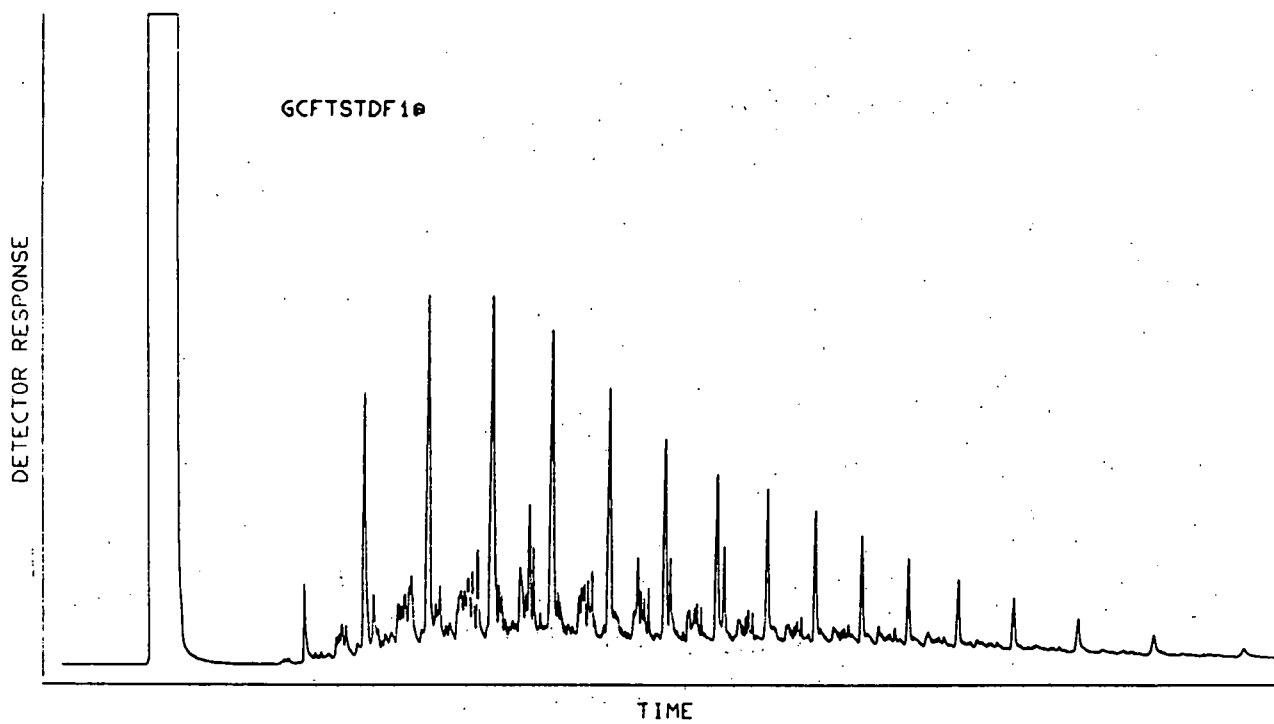


Figure 7.4.78 GC of Aromatic Fraction of Neat Oil

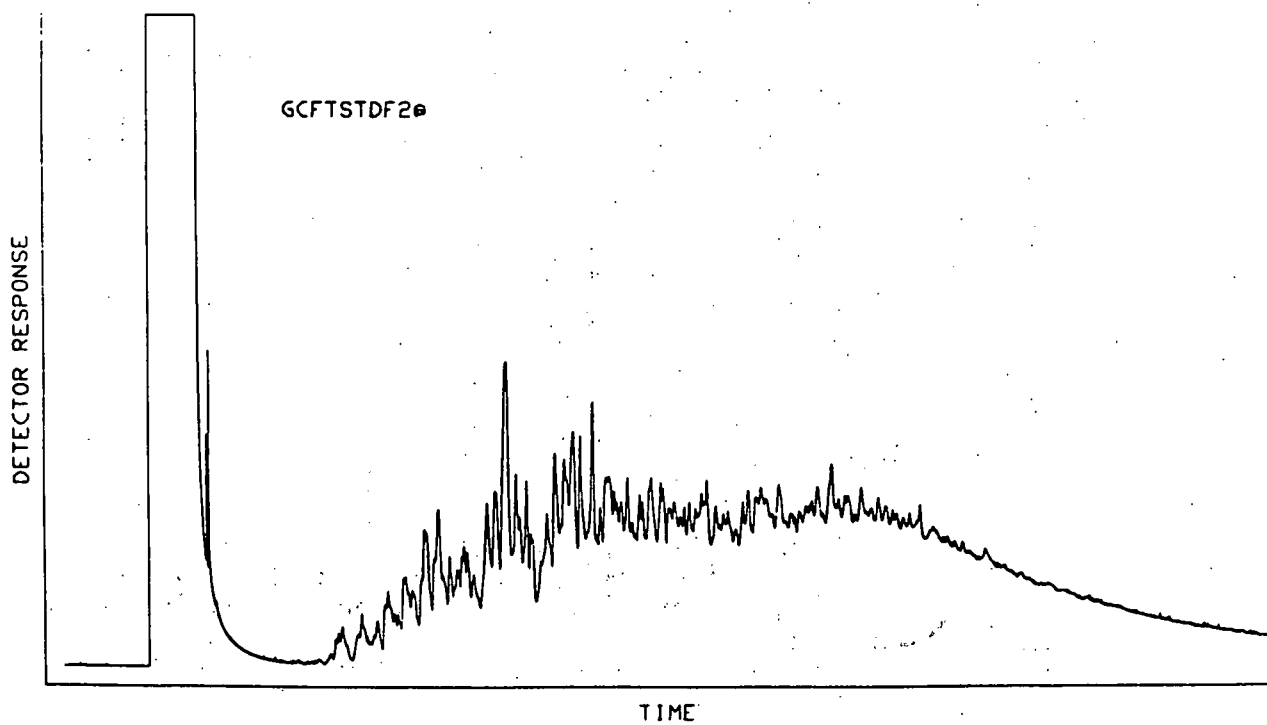


Figure 7.4.79 GC of Polar Fraction of Neat Oil

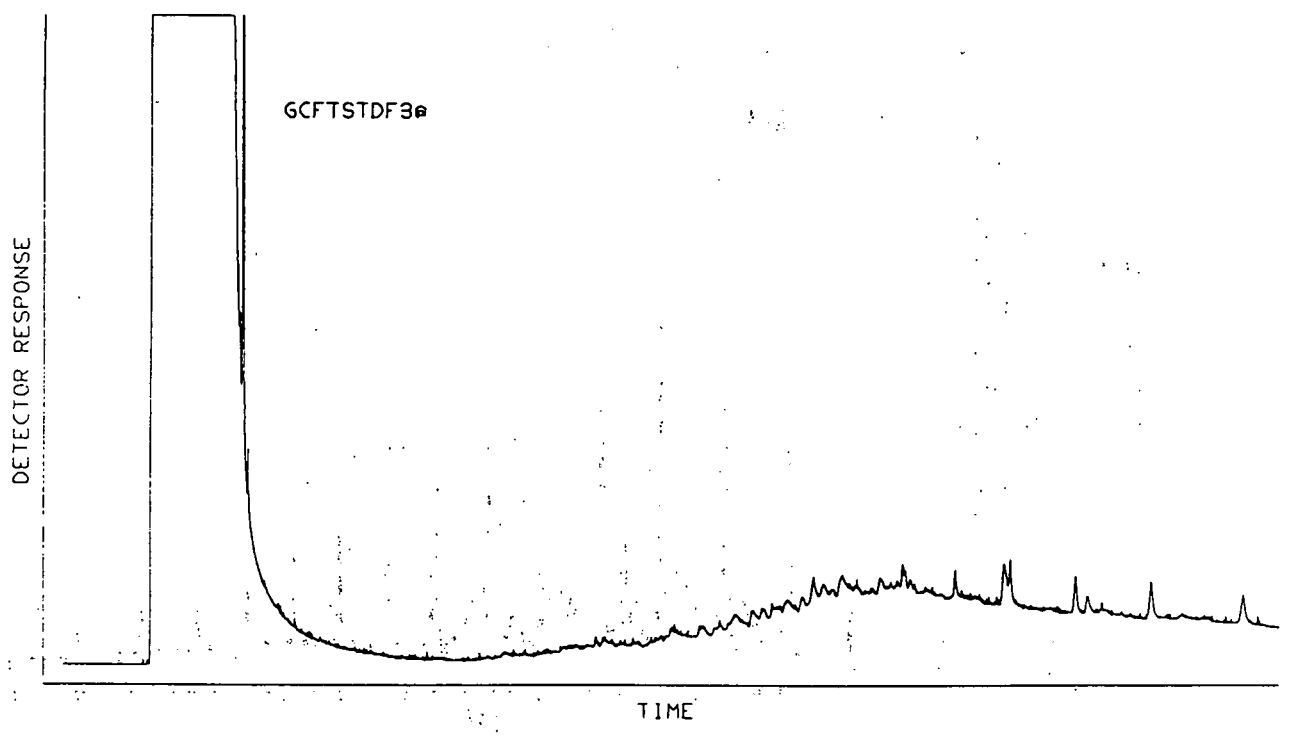


Figure 7.4.80 GC of Paraffin Fraction From Oil Tank at 24 hrs.

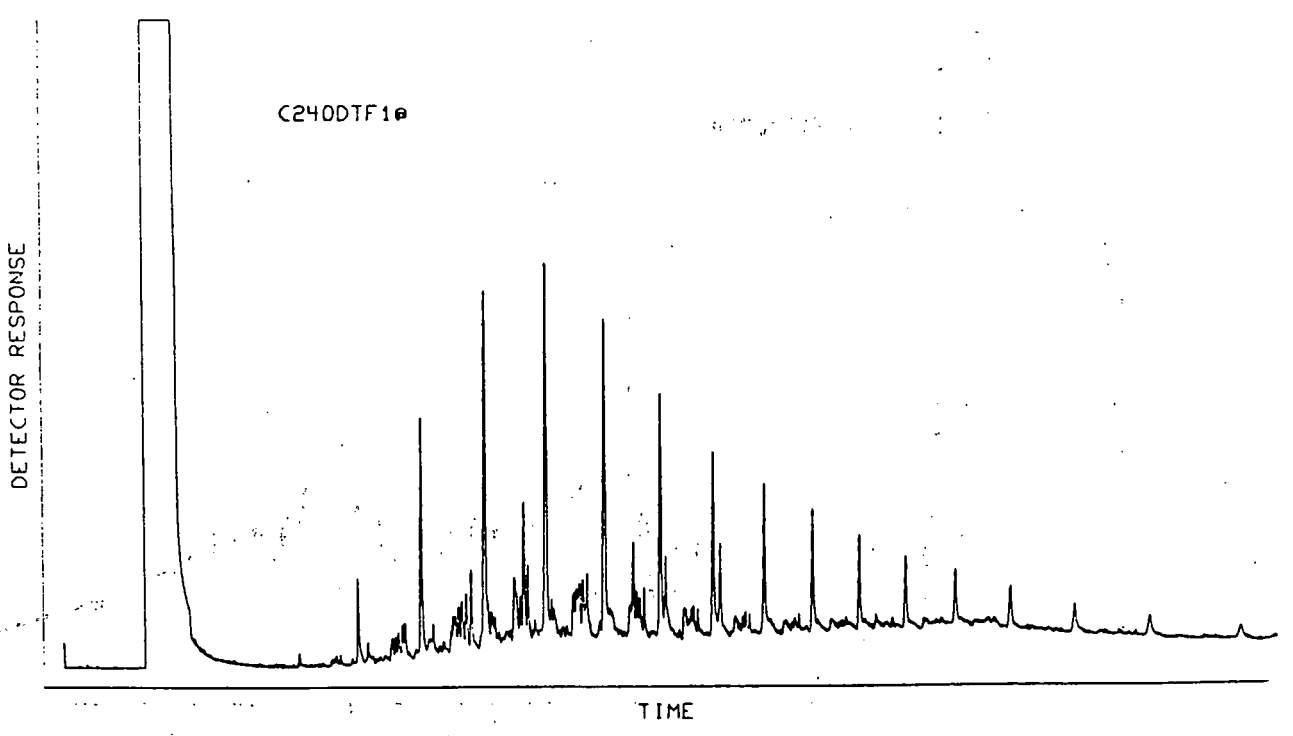


Figure 7.4.81 GC of Aromatic Fraction From Old Tank at 24 hrs.

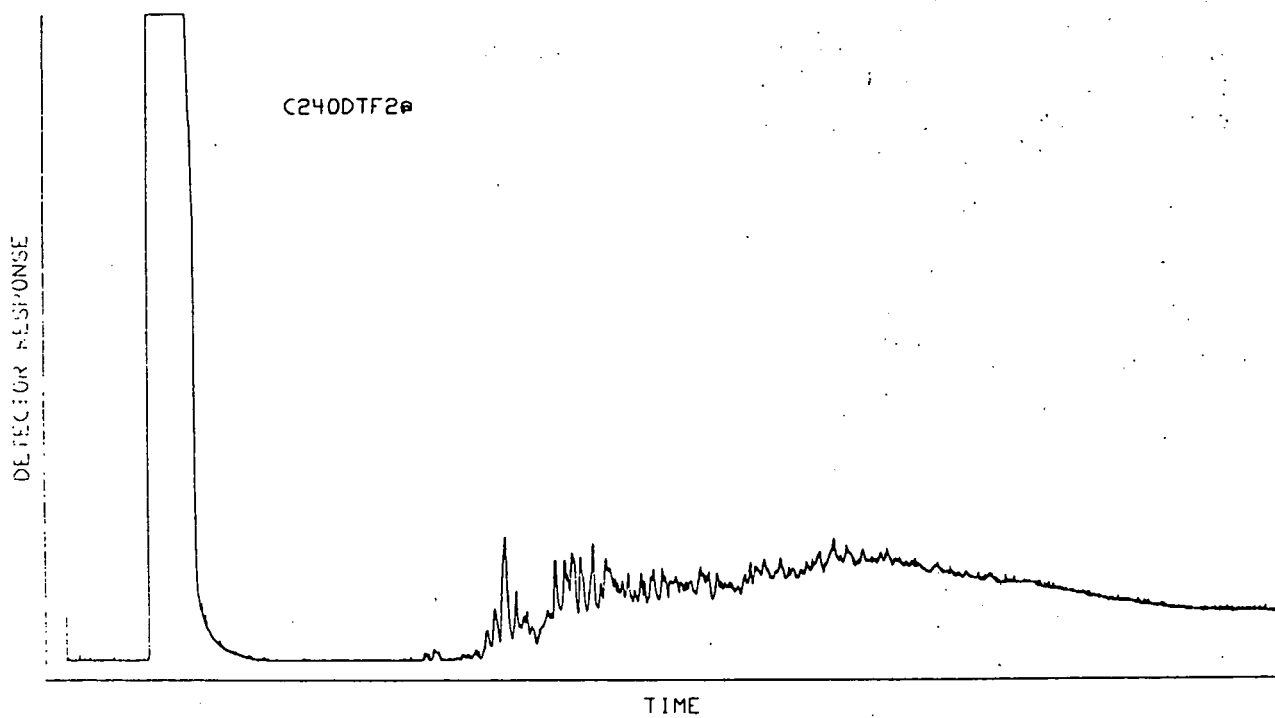
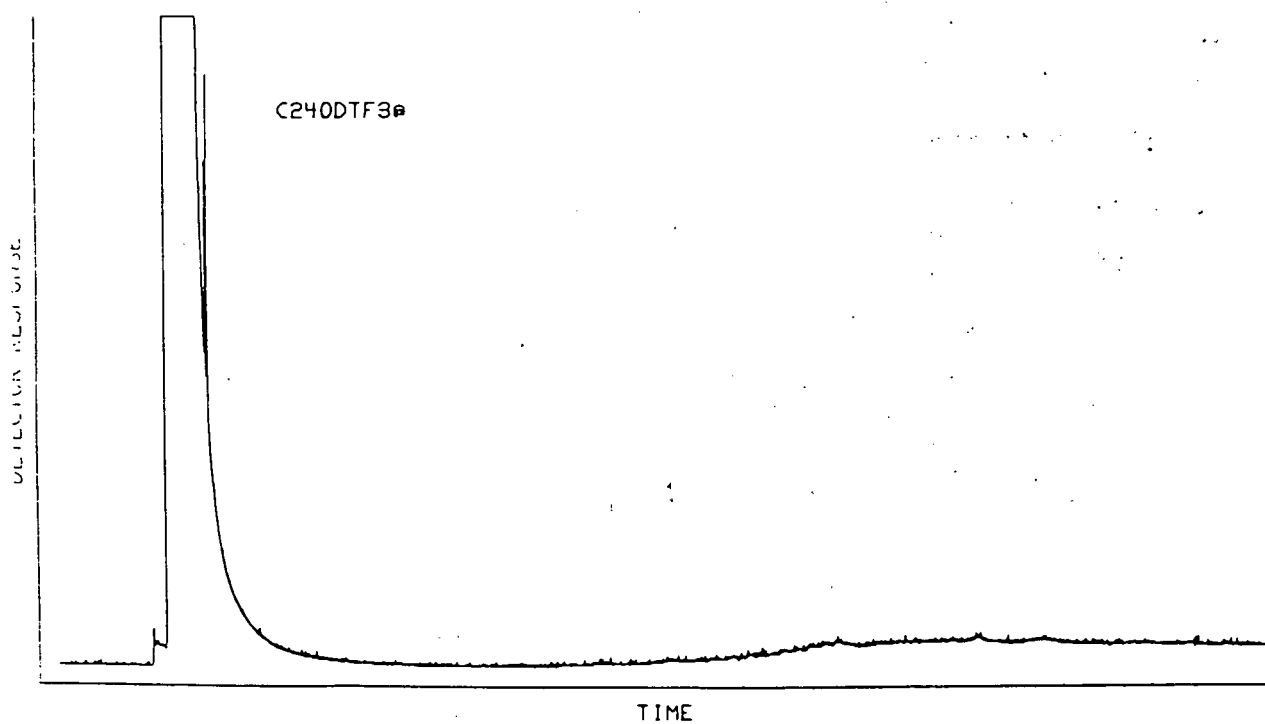


Figure 7.4.82 GC of Polar Fraction From Old Tank at 24 hrs.



The fractions of the sample from the middle of the tank (Figures 7.4.83 and 7.4.84) at 24 hours contained larger relative amounts of the isoprenoids, pristane and phytane, in the paraffin phase, but very small peaks in the aromatic phase. This suggests (but is not conclusive evidence) that aromatics are stratified in the water column and remain near the top of the tank, indicating that the dispersant has a different effect on paraffins and aromatics.

The GC of the paraffin fraction at 48 hours (Figure 7.4.85) shows an odd/even effect with the even chain lengths ($n\text{-C}_{16}$, $n\text{-C}_{18}$ and $n\text{-C}_{20}$) found at higher concentrations than the odd chain lengths. This odd/even effect is less pronounced in the GC of the composite sample (Figure 7.4.64); however, the distribution in the GC of the composite is affected by the large unresolved envelope centered at $n\text{-C}_{15}$.

The remaining GC of the fractionated samples do not reveal any new features that are not observed in the GC of the composite samples.

(3) Conclusions

In this experiment, useful conclusions can be drawn from the gas chromatograms of samples from the oil dispersant tank. As shown by the quantitative results from this experiment and from previous experiments, the oil (petroleum hydrocarbons) appear to migrate with time to the bottom of the tank. This is supported by the gas chromatograms. However, in this experiment, the chromatograms show that not all of the components of the oil appear equally distributed at all three sampling levels. At 1 and 24 hours more of the lighter components ($\text{C}_{10}\text{-C}_{12}$) are found in the sample from the top port. The fractionation procedure indicates that the heavier aromatics never reach the center of the tank.

After 192 hours there appears to be more of the lower molecular weight paraffins in the bottom of the tank than at the other two levels. This could reflect greater degradation of the heavier paraffins at the bottom. In the same way, there is a general increase in the relative amounts of the isoprenoids, pristane and phytane, as a function of time; this could also be due to the degradation of the normal paraffins with time.

III. References

1. Jasper, W.J., Kim, T.J., Wilson, M.P., "Drop-size Distribution in a Treated Oil Water System," ASTM Conference, Chemical Dispersants, Williamsburg, Pa., 1977.
2. Traxler, R.W., Bhattacharya, L.S., "Effect of Chemical Dispersants on Microbial Utilization of Petroleum Hydrocarbons," ASTM Conference, *ibid.*
3. Wilson, M.P., "The Assessment Problems of Whether or Not to Treat Oil Spills," *ibid.*
4. Brown, R.A., Elliott, J.J., Searl, T.D., "Measurement and Characterization of Nonvolatile Hydrocarbons in Ocean Water," AID. 4BA.74 (1974).

Figure 7.4.83 GC of Paraffin Fractions From Middle of Old Tank at 24 hrs.

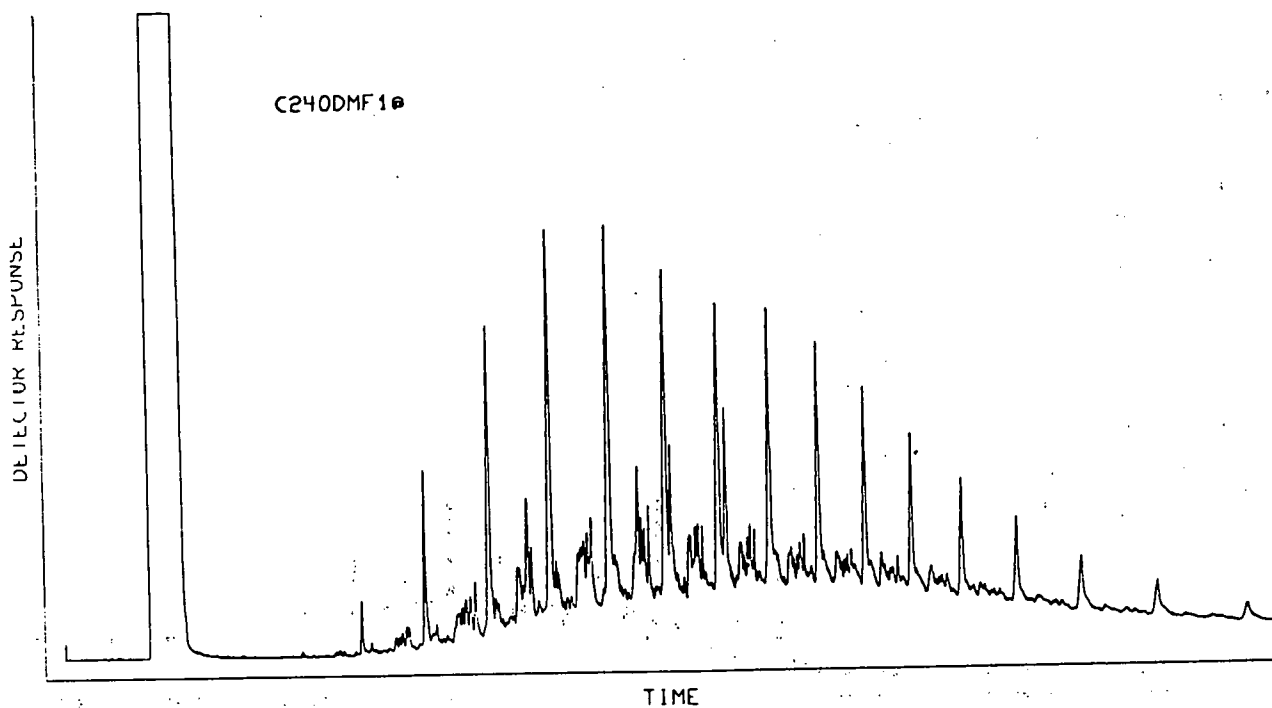


Figure 7.4.84 GC of Aromatic Fractions From Middle of Old Tanks at 24 hrs.

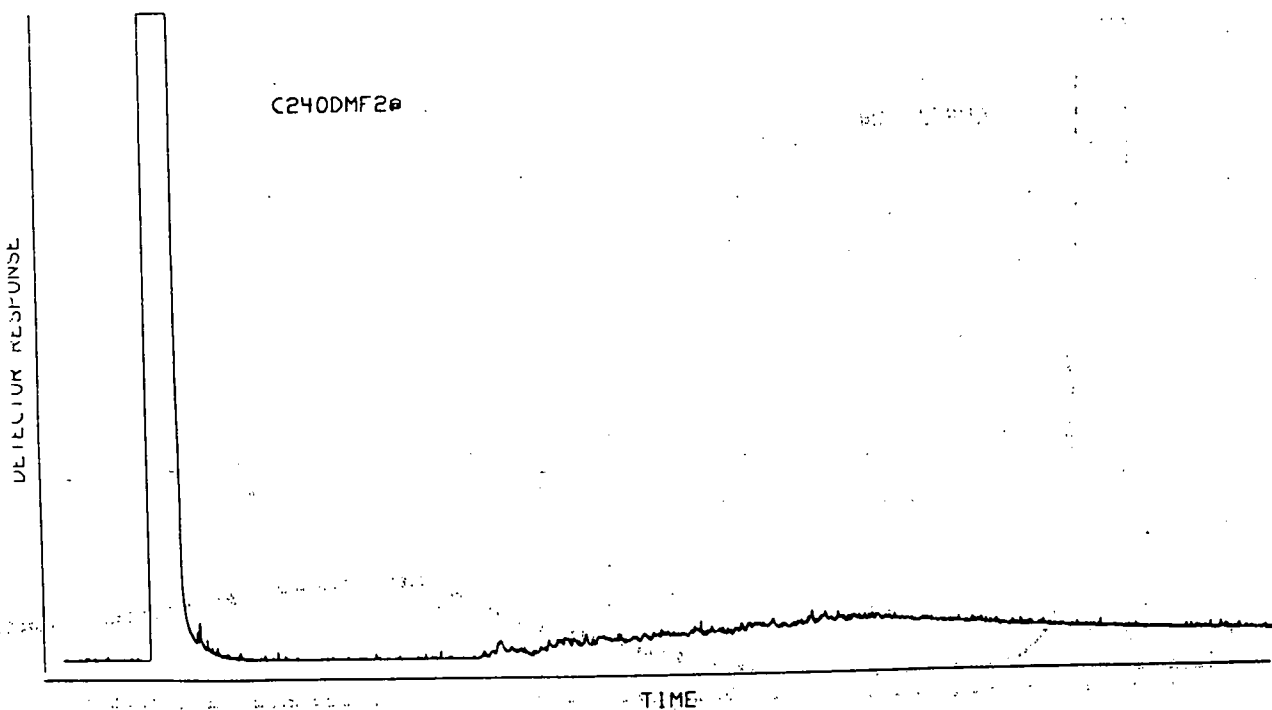


Figure 7.4.85 GC of Paraffin Top Fraction at 48 hrs.

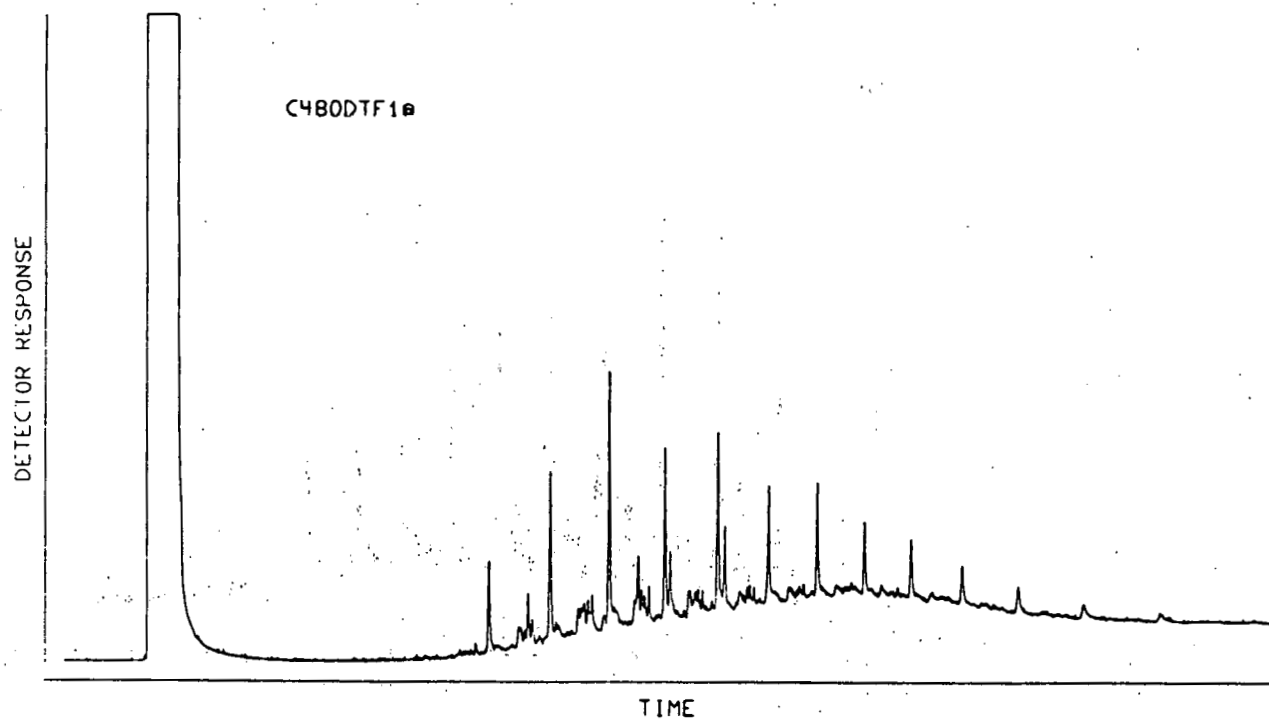


Figure 7.4.86 GC of Aromatic Top Fraction at 48 hrs.

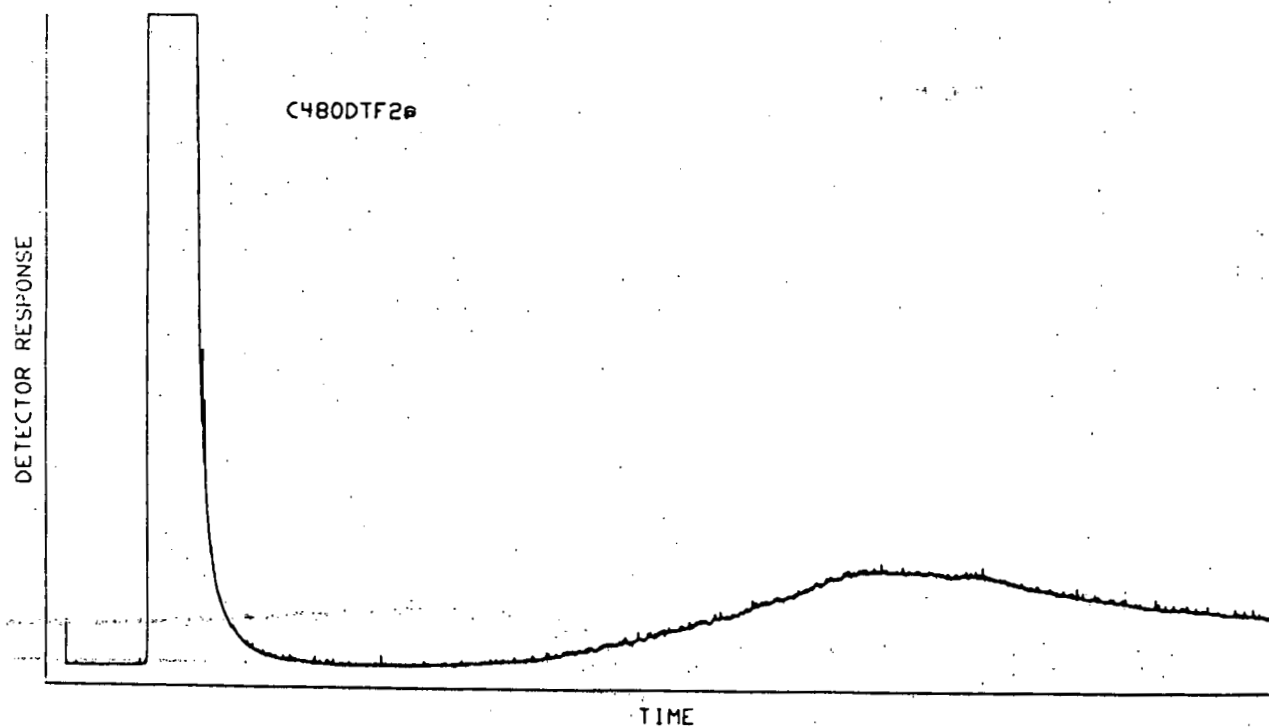


Figure 7.4.87 GC of Polar Fraction Top Fraction at 48 hrs.

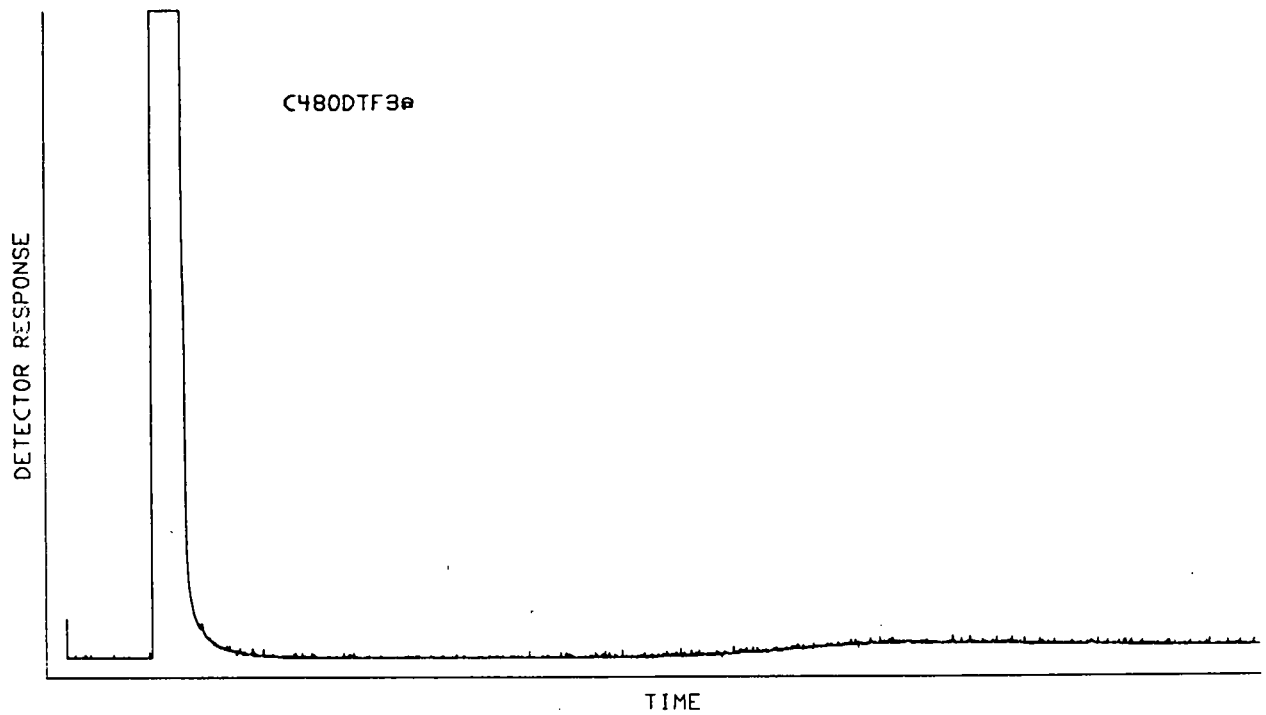


Figure 7.4.88 GC of Paraffin Middle Fraction at 48 hrs.

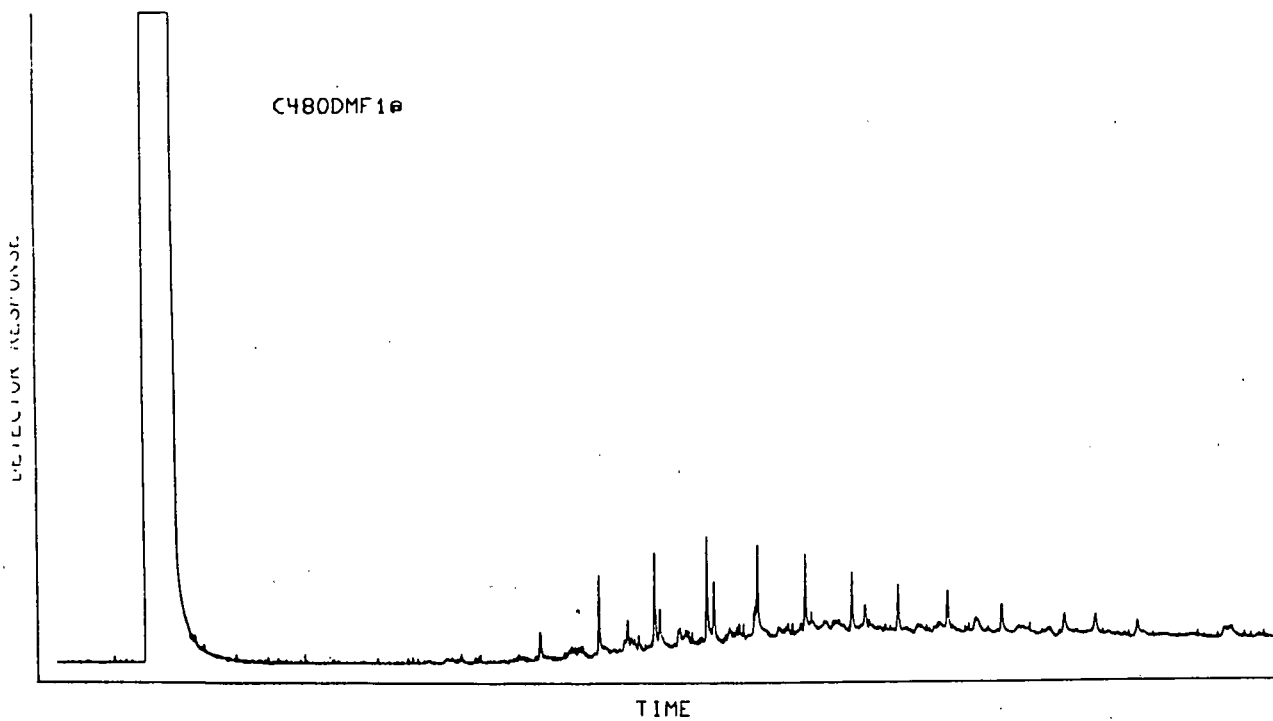


Figure 7.4.89 GC of Aromatic Middle Fraction at 48 hrs.

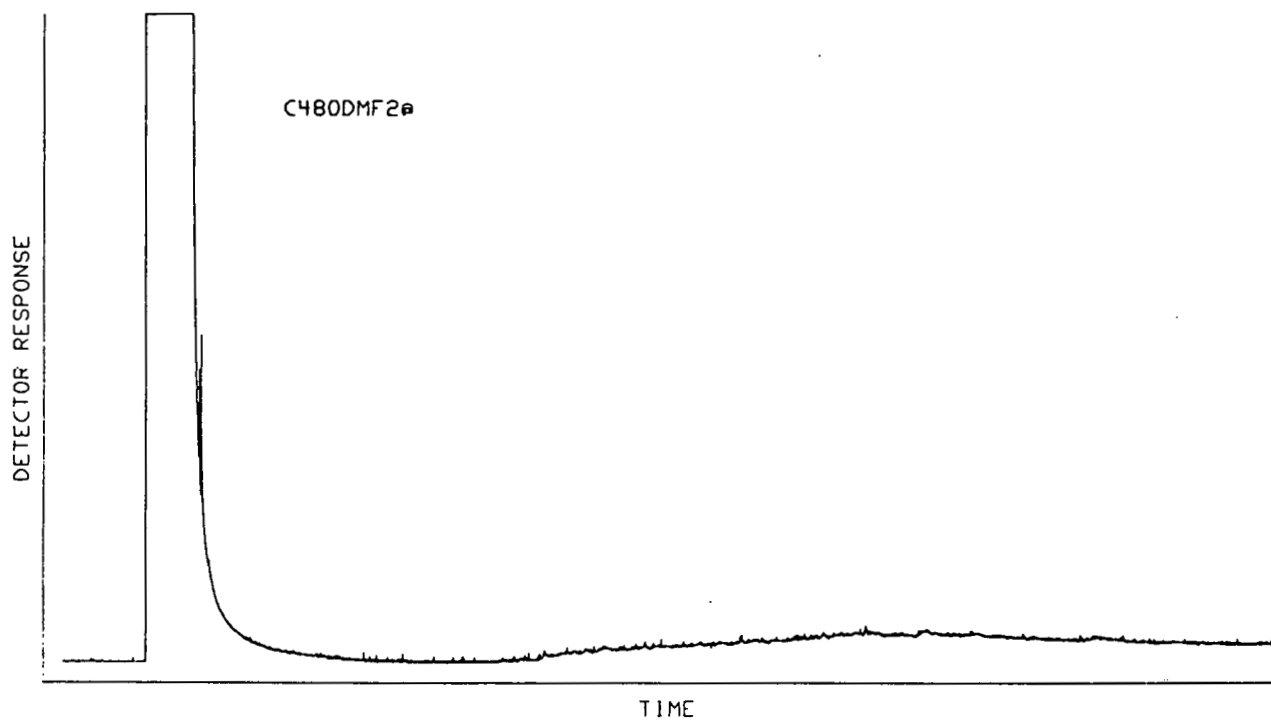


Figure 7.4.90 GC of Paraffin Top Fraction at 72 hrs.

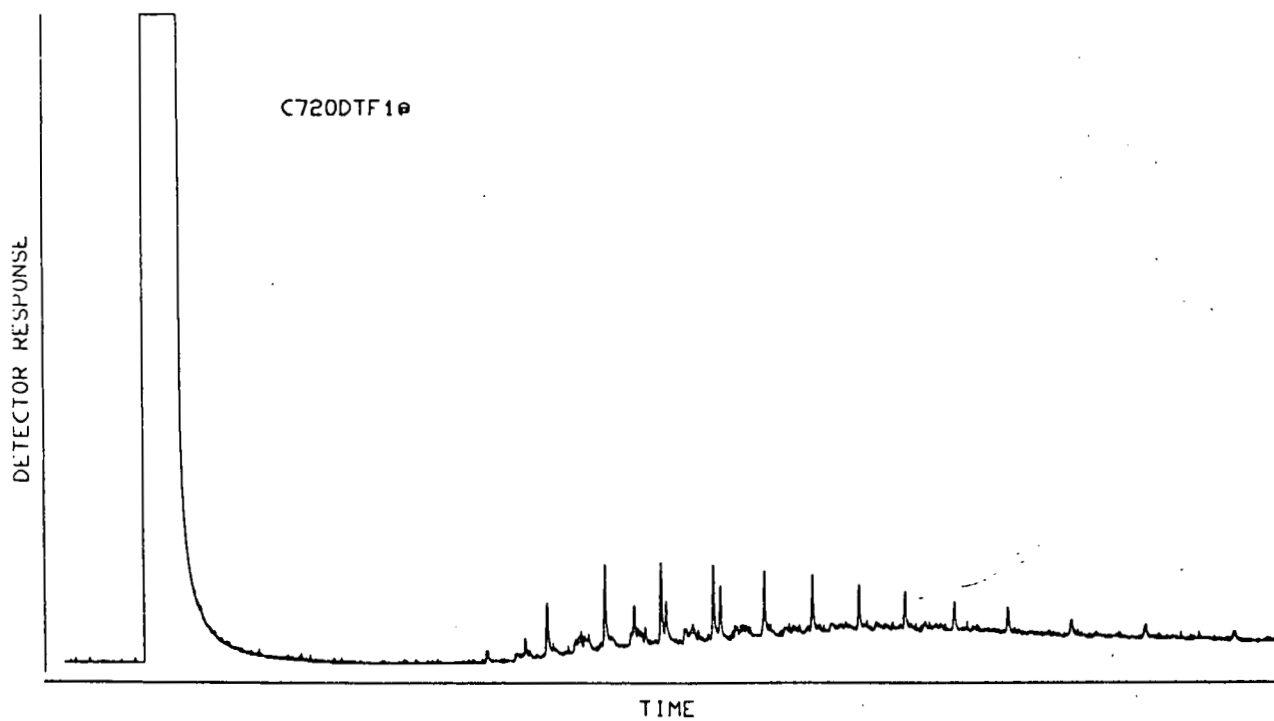


Figure 7.4.91 GC of Polar Top Fraction at 72 hrs. 7-128

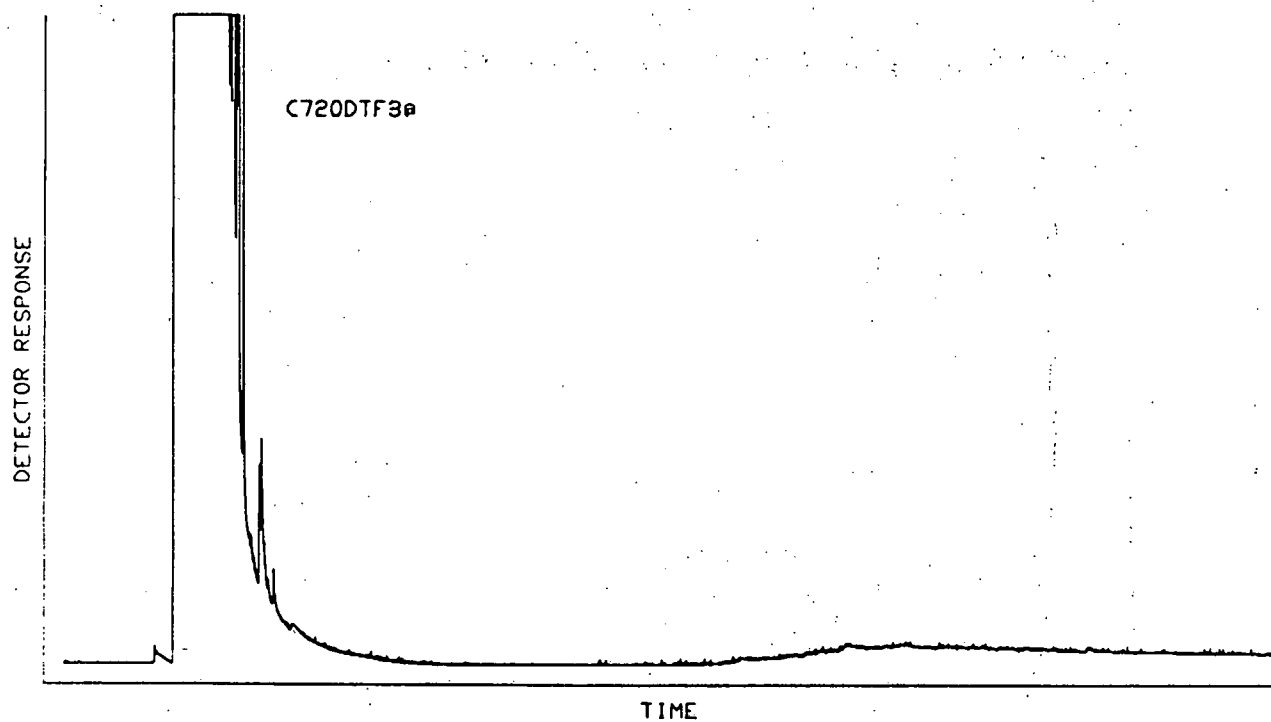


Figure 7.4.92 GC of Aromatic Middle Fraction at 72 hrs.

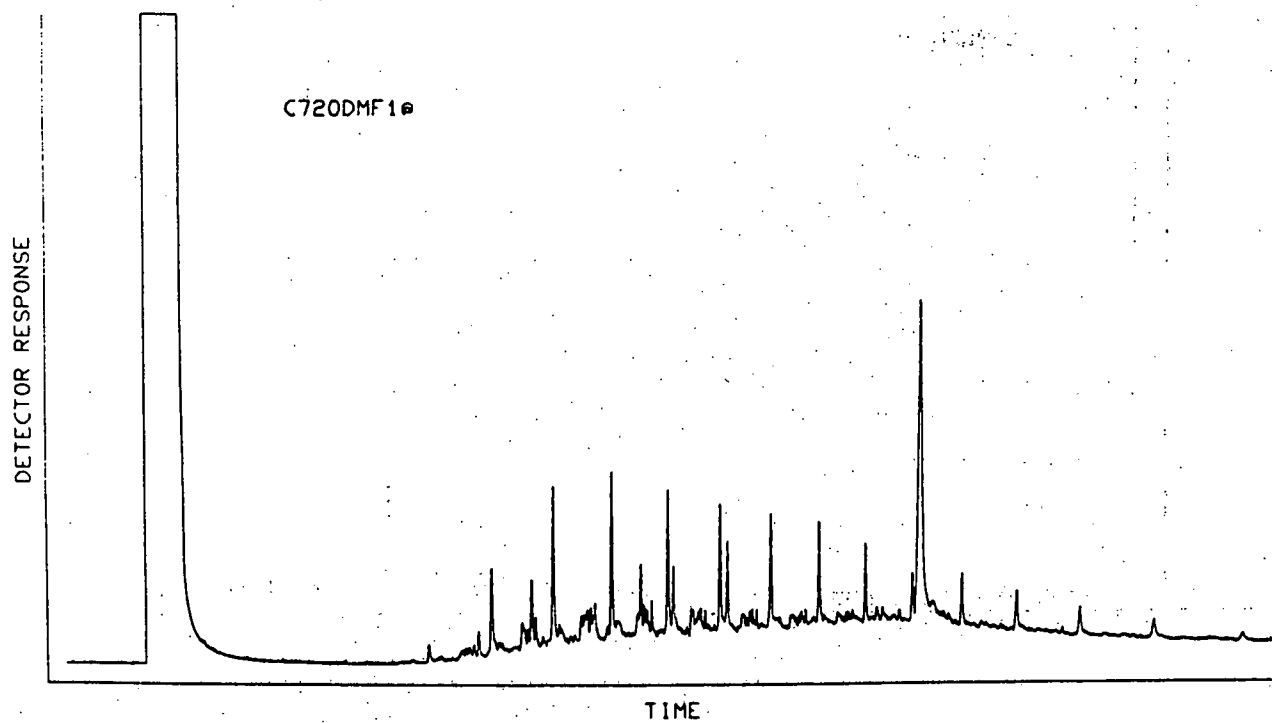


Figure 7.4.93 GC of Paraffin Middle Fraction at 72 hrs.

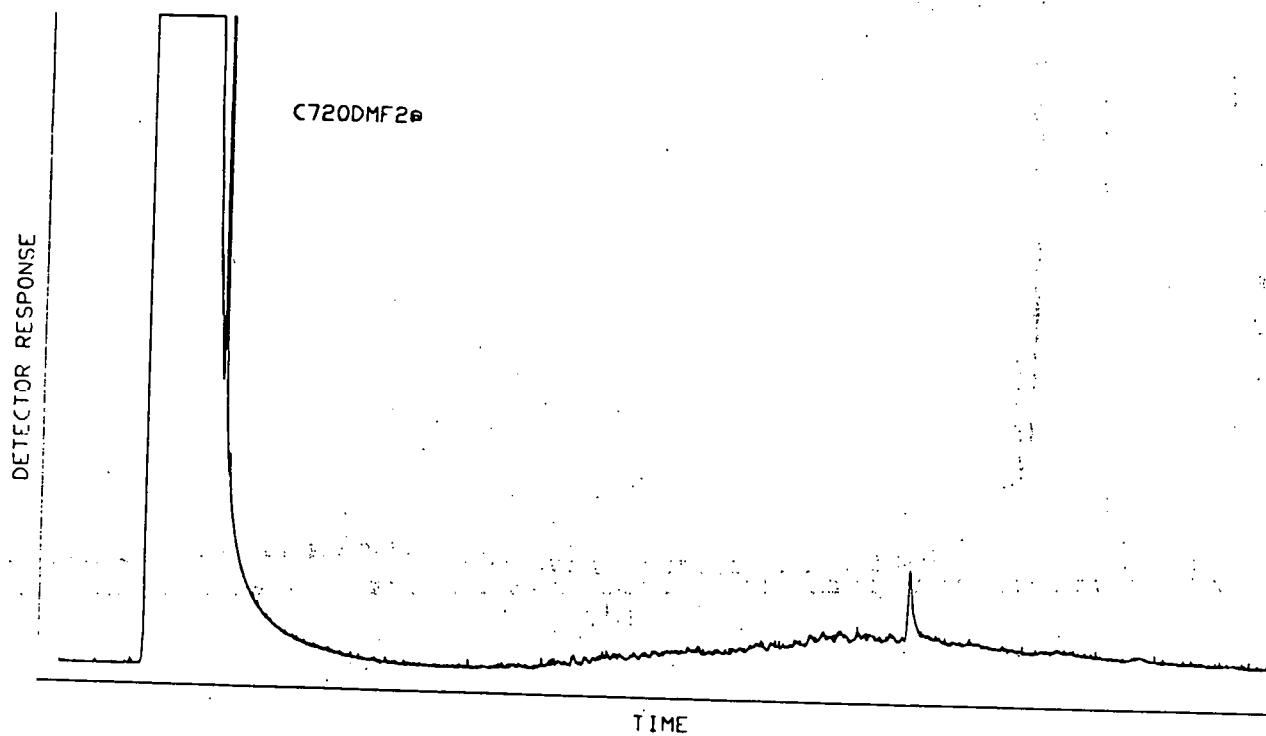
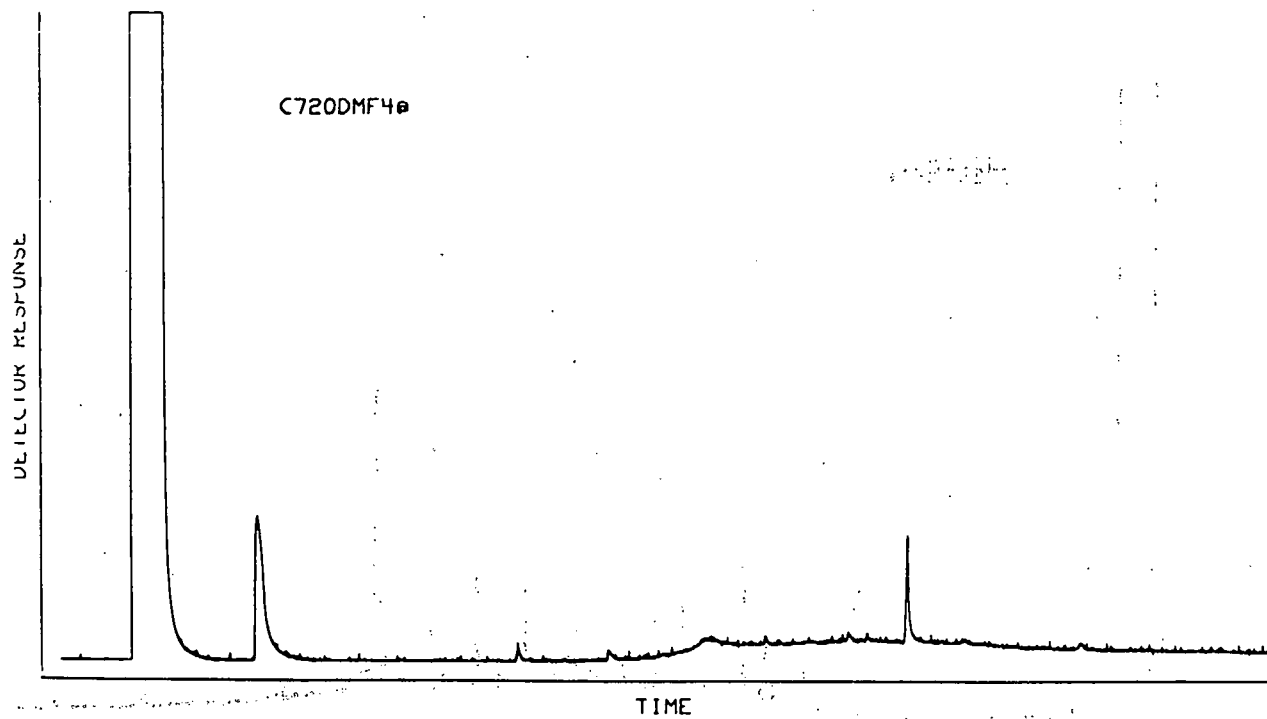


Figure 7.4.94 GC of Polar Middle Fraction at 72 hrs.



7.5 Jerusalem Flow Thru Experiment

7.5.1 Introduction

The flow-thru experiment consisted of four 55 gallon drums with sea water flowing through each at the rate of 10 gallons/hour. Initially, the following components were added to the surface of the sea water:

- 1) Control
- 2) Ten ml of dispersant (Corexit 9527)
- 3) Two hundred ml oil (Kuwait crude)
- 4) Two hundred ml of Kuwait crude and 10 ml of Corexit 9527

Water samples were collected every week from the top, middle and bottom of each tank. Sediment samples were collected from tanks 1, 3, and 4 at week 1 (first day of the experiment) and week 4.

7.5.2 Experimental

(A) Quantitative Analysis of Water Samples

One-liter water samples were extracted with two 15 ml aliquots of CS₂. The aliquots were combined and the volume adjusted to 25 ml. The infrared spectrum was recorded from 3200 to 2800 cm⁻¹ using 6 mm AgCl matched cells, and the absorbance of the C-H stretching band at 2930 cm⁻¹ was used to determine the concentration of extractable organics from plots of concentration vs. absorbance measured using known amounts of the Kuwait crude oil, Kuwait and Corexit, or Corexit. An extraction efficiency of 65% (previously determined) was used for samples from tanks 1, 3 and 4. An extraction efficiency of 22% was used for tank 2 (dispersant) when it was found that the dispersant was present in the extract by qualitative infrared spectroscopy; however, if the dispersant was not present, a 65% efficiency was used.

(B) Qualitative Analysis of Water Samples Collected from the Tanks.

During the 1st, 4th and 6th weeks, 3.5 liter water samples were collected from the tanks. These larger samples were collected in order to perform complete qualitative analyses. The samples from the fourth week did not contain enough hydrocarbons to warrant qualitative analysis; however, samples from the other two weeks were analyzed.

All samples were extracted with CS₂ and the extracts concentrated to 1 or 2 ml. Infrared spectra between 1950 and 660 cm⁻¹ were measured using 6 mm AgCl cells. After measuring the infrared spectra, the CS₂ was completely removed from each of the extracts by evaporation and the residue was taken up in 20 μ l of hexane. Two μ l samples were injected into a gas chromatograph equipped with a glass capillary column (Supelco SP 2100). Three samples were also separated into multiple fractions containing aliphatics, small and large ring aromatics and polar components using a column of alumina and eluting with pentane, toluene and methanol. Each fraction was analyzed on a glass capillary column GC.

(C) Analysis of Sediment Samples

Sediment samples were subjected to a saponification-extraction using a KOH-toluene-methanol reflux. The organic layer was collected and passed through a silica gel column to remove natural polar components. Both qualitative and quantitative infrared spectra of the extracts were measured. The extracts were further separated by thin-layer chromatography and all of the hydrocarbons running above the standard, phenanthrene, were dissolved in hexane and injected into the capillary column gas chromatograph.

7.5.3 Results

(A) Qualitative GC of Water Samples

(a) Week One

Water samples were collected one hour after addition of the oil and dispersant.

i. Control Tank

Gas chromatograms of water samples from the top, middle and bottom of the control tank are shown in Figures 7.5.1, 2 and 3. Gas chromatograms of the top and bottom (CT and CB) suggest the presence of normal paraffins from n-C₁₆ to n-C₂₄, which is indicative of petroleum.

ii. Dispersant Tank

GC of the top, middle and bottom water extracts are shown in Figures (7.5.4, 5 and 6). A number of relatively intense peaks are observed in all three GCs; however, peaks at short retention times found in the GC of the oil/dispersant (Figure 7.5.10) are not observed.

iii. Oil Tank

GC of extracts of water from the top, middle and bottom of the oil tank are shown in Figures 7.5.7, 8 and 9. A number of relatively intense peaks are observed in the GC of the top sample. The normal paraffin peaks are relatively weak compared to the other components which suggests that the more soluble aromatics and polar compounds are present. Two prominent peaks are observed in the GC of the middle sample and these two peaks are also present in the GC of the top sample.

iv. Oil/Dispersant Tank

GC of the extracts of water from the top and bottom of the oil/dispersant tank are shown in Figures 7.5.10 and 11; the extract of the middle sample was accidentally destroyed during the analysis procedure. The GC of the top samples is typical of weathered oil with the addition of two peaks at short retention times and several broad peaks at longer retention times; these peaks are undoubtedly due to the dispersant. The interesting feature is that the dispersant takes most of the unweathered components of oil into the water column.

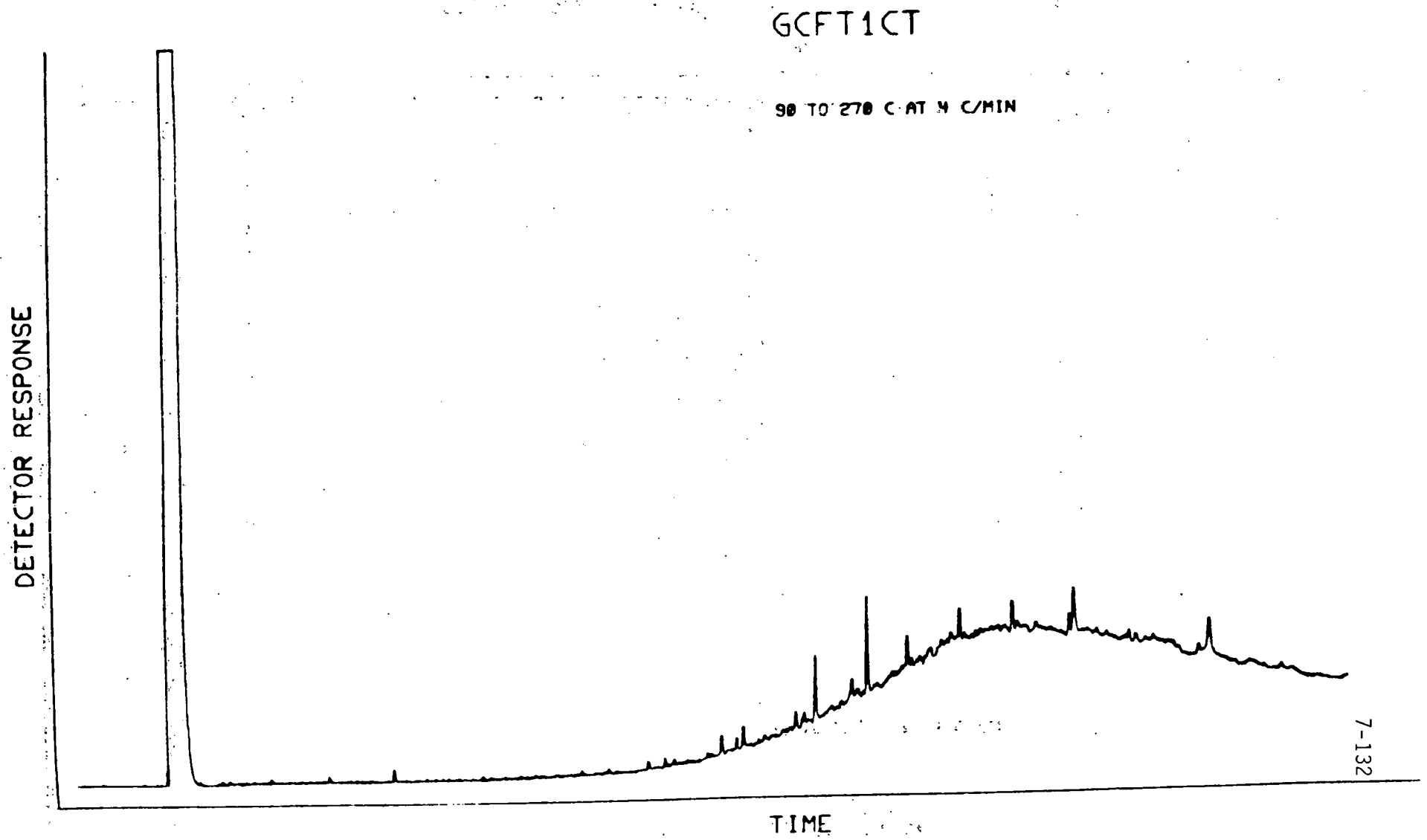


Figure 7.5.1 GC of the Control Tank, top, 1 hr.

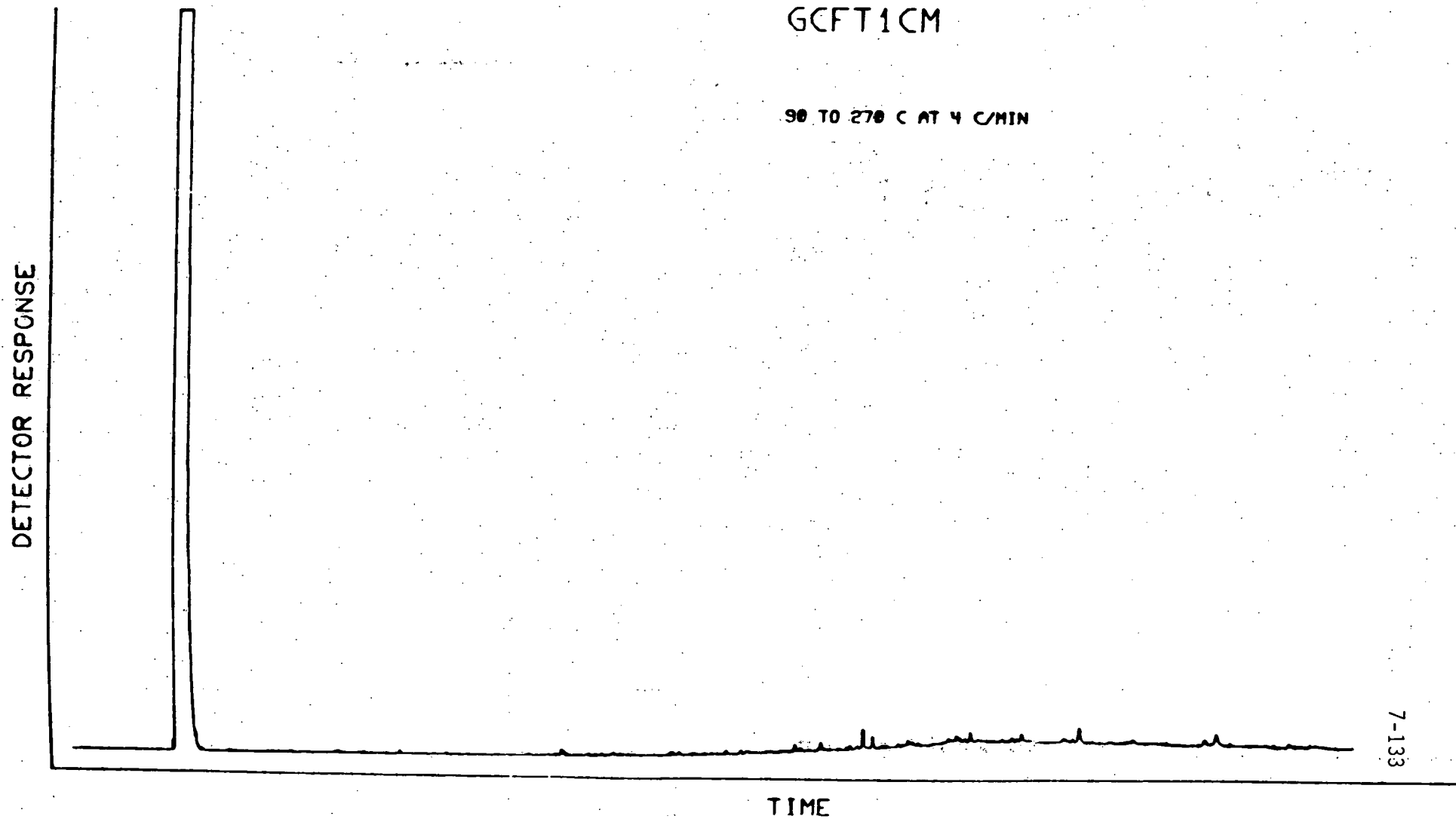


Figure 7.5.2 GC of the Control Tank, middle, 1 hr.

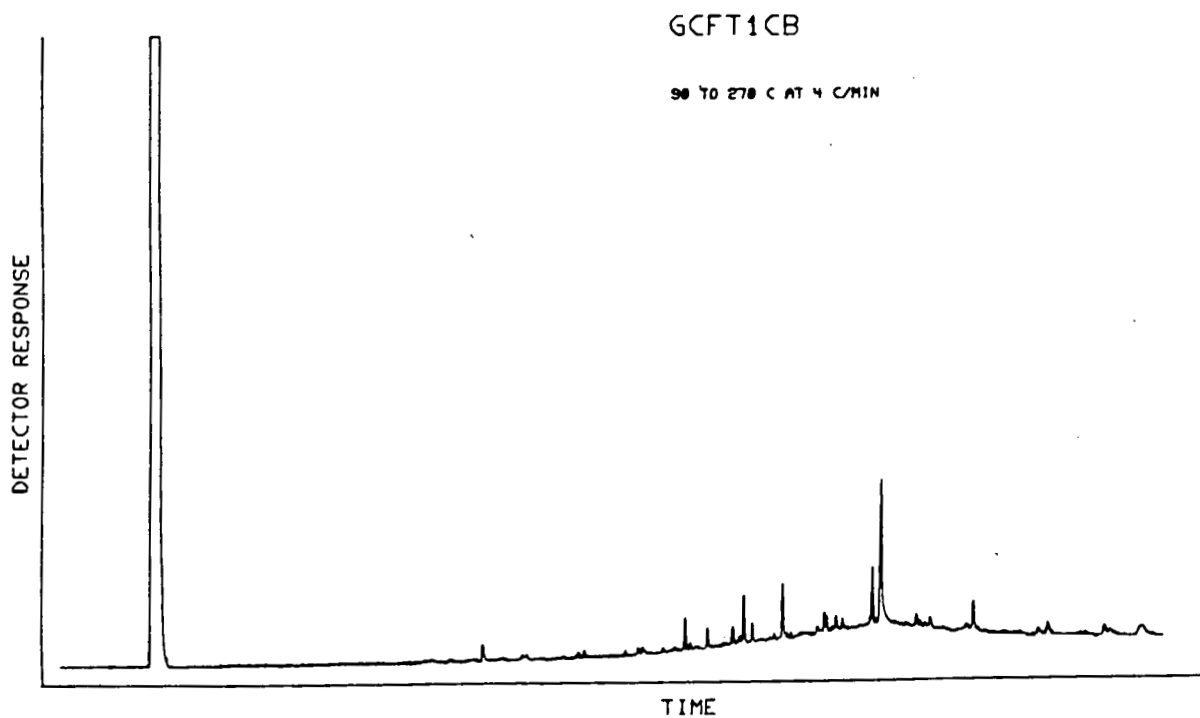


Figure 7.5.3 GC of the Control Tank, bottom, 1 hr.

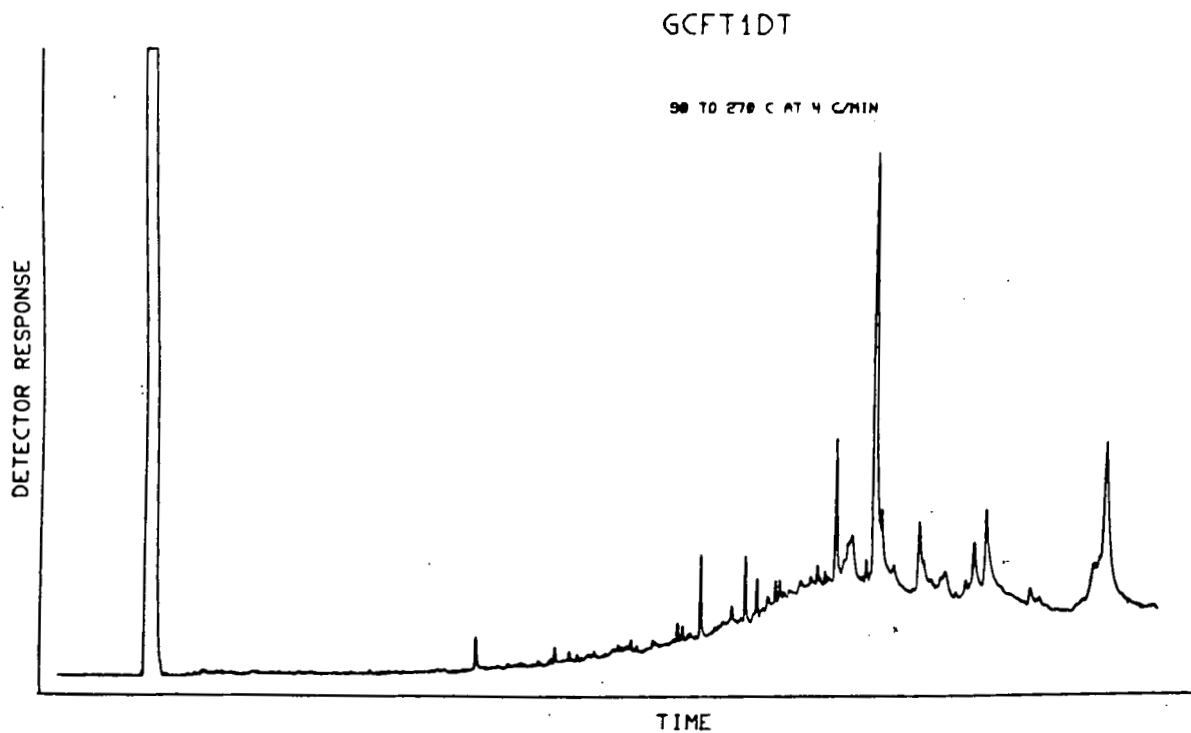


Figure 7.5.4 GC of the Dispersant Tank, top, 1 hr.

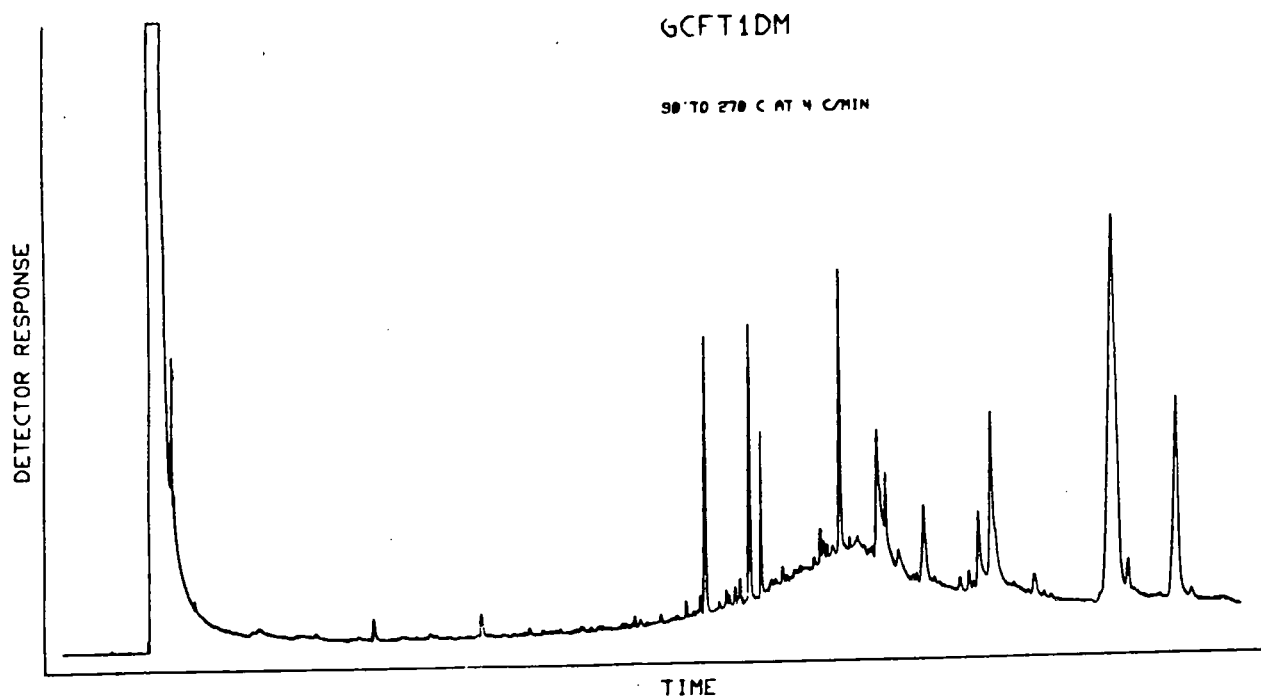


Figure 7.5.5 GC of the Dispersant Tank, middle, 1 hr.

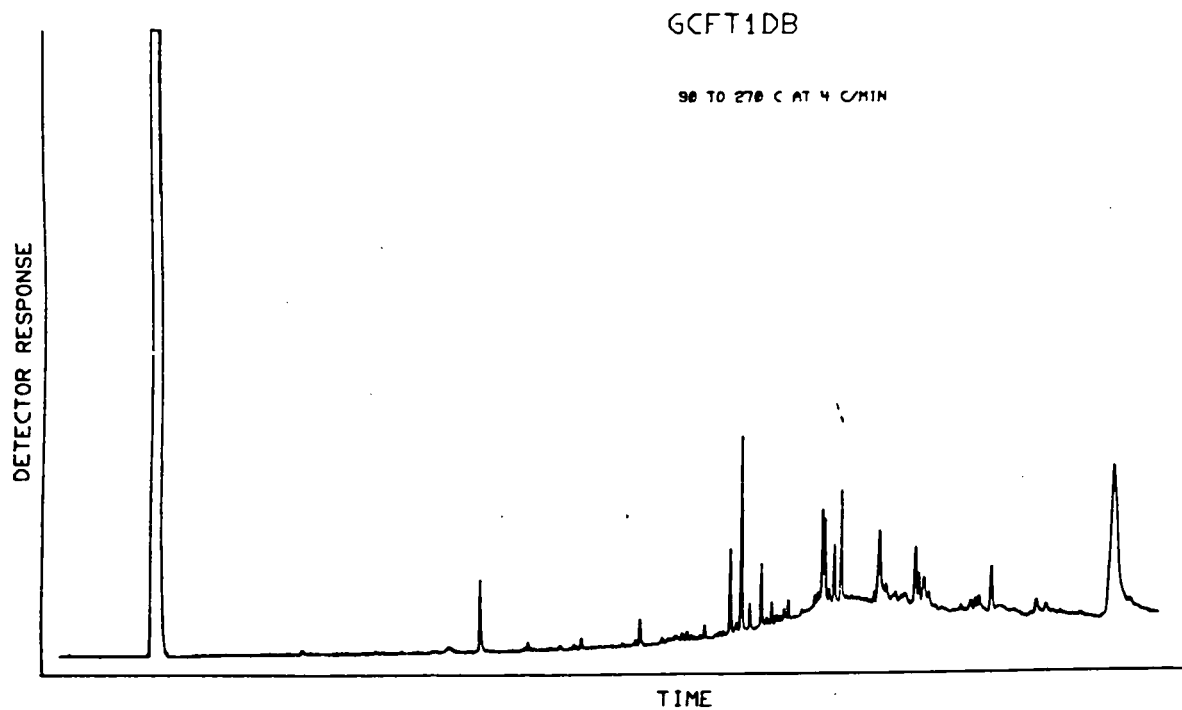


Figure 7.5.6 GC of the Dispersant Tank, bottom, 1 hr.

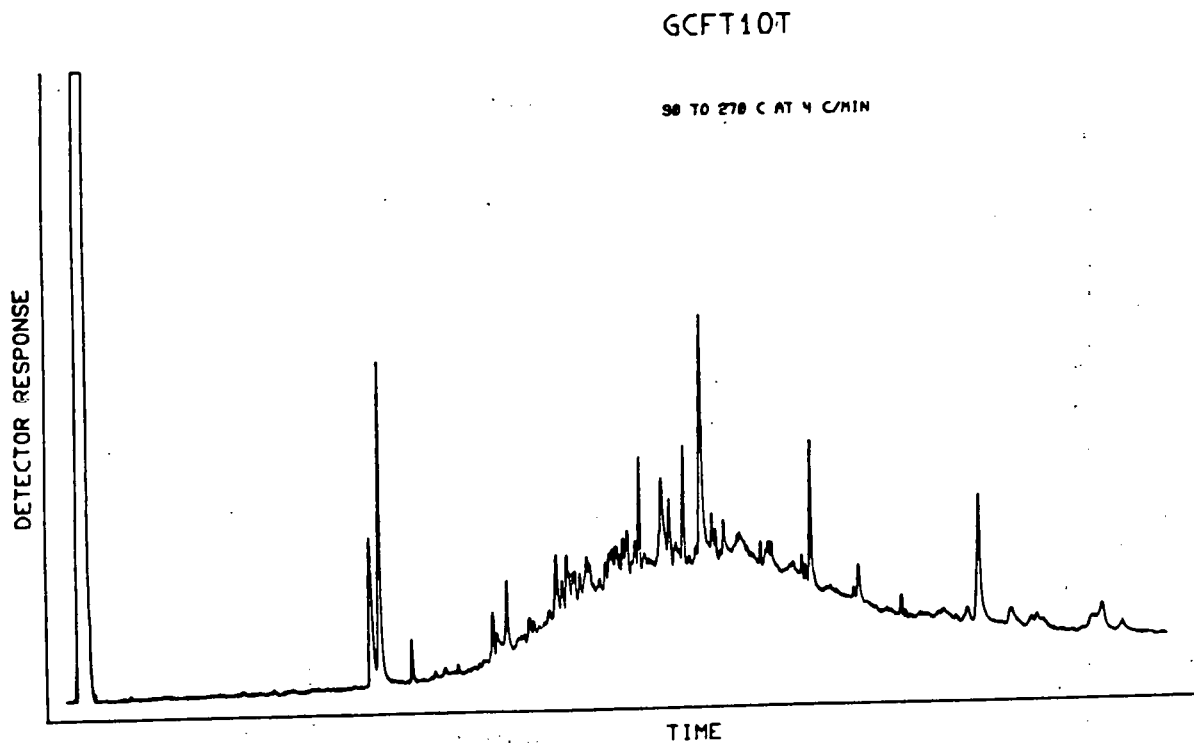


Figure 7.5.7 GC of the Oil Tank, top 1 hr.

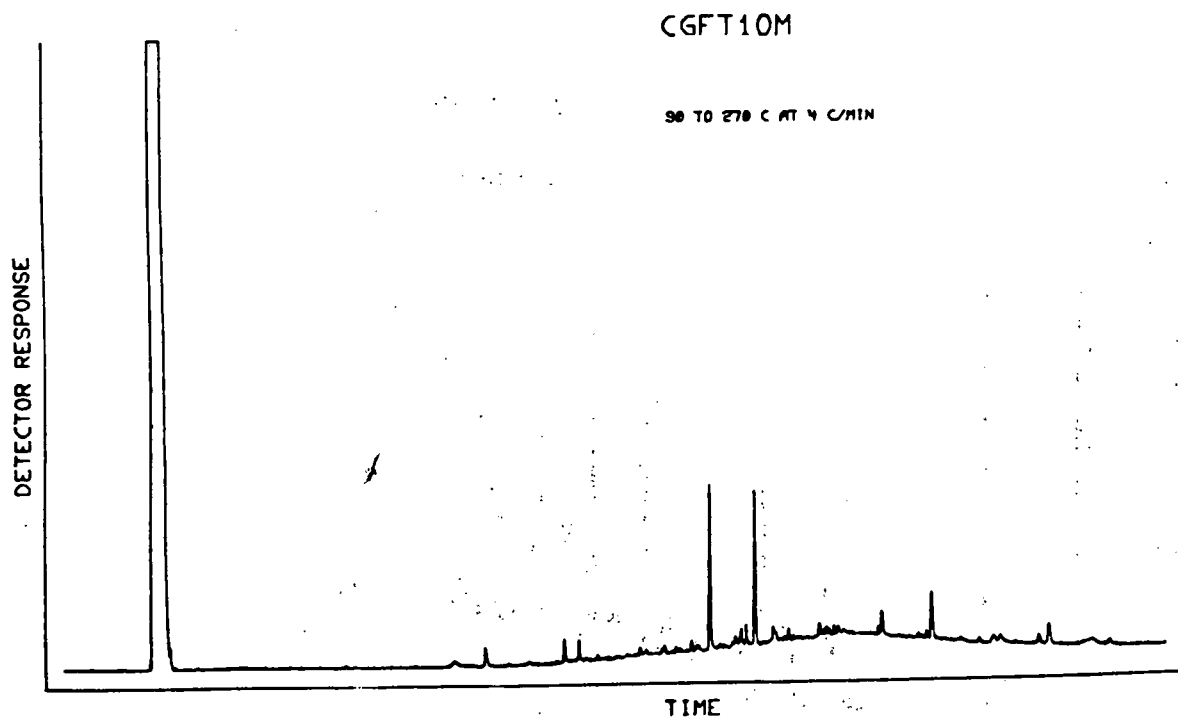


Figure 7.5.8 GC of the Oil Tank, middle, 1 hr.

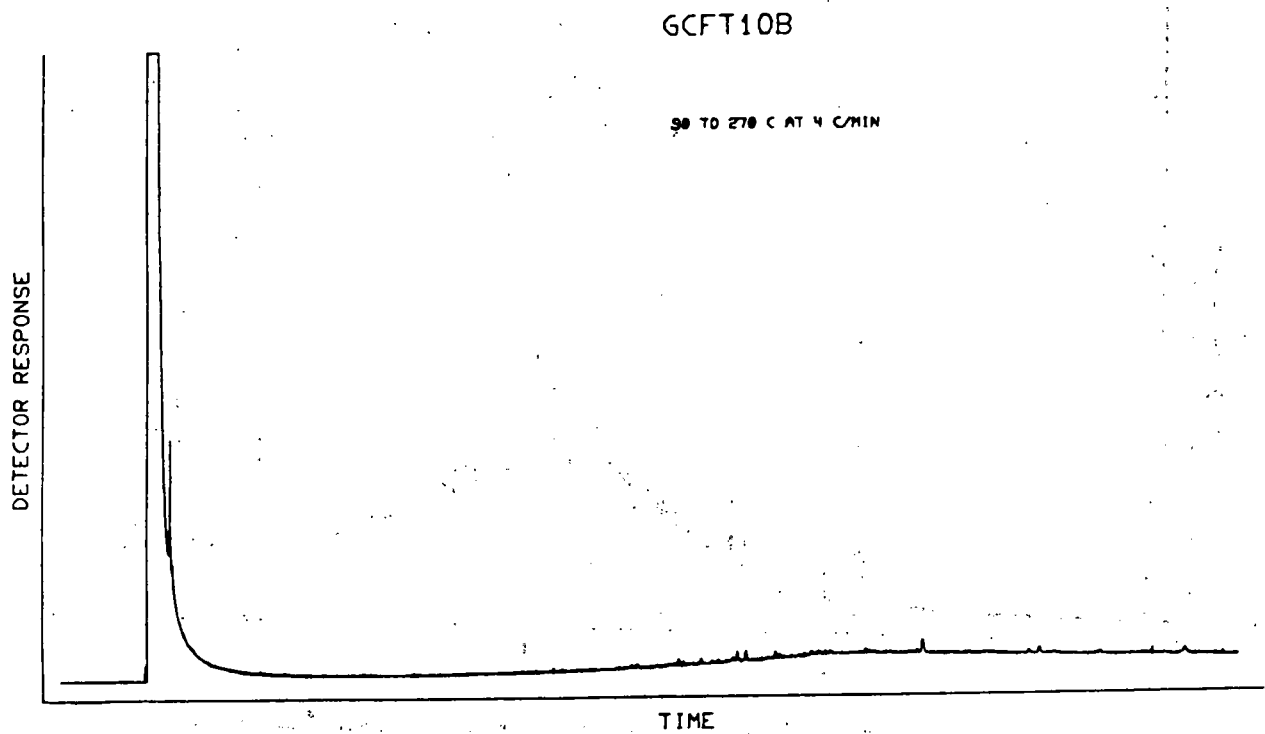


Figure 7.5.9 GC of the Oil Tank, bottom, 1 hr.

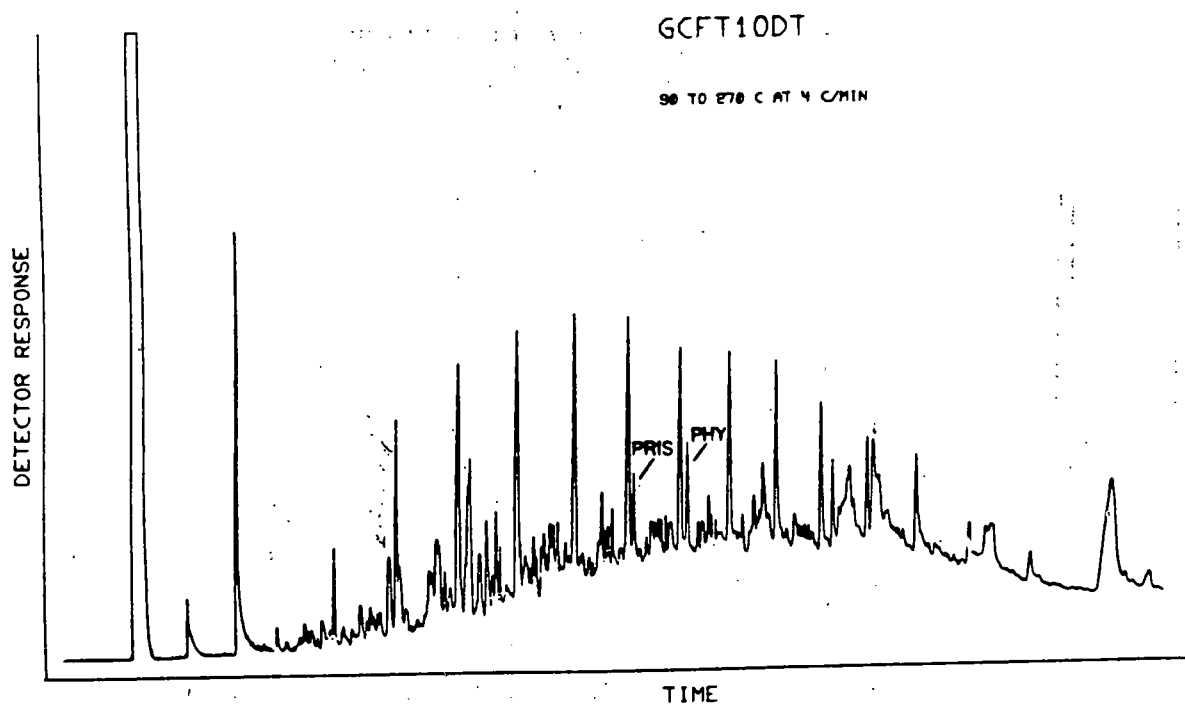


Figure 7.5.10 GC of the Oil/Dispersant Tank, top, 1 hr.

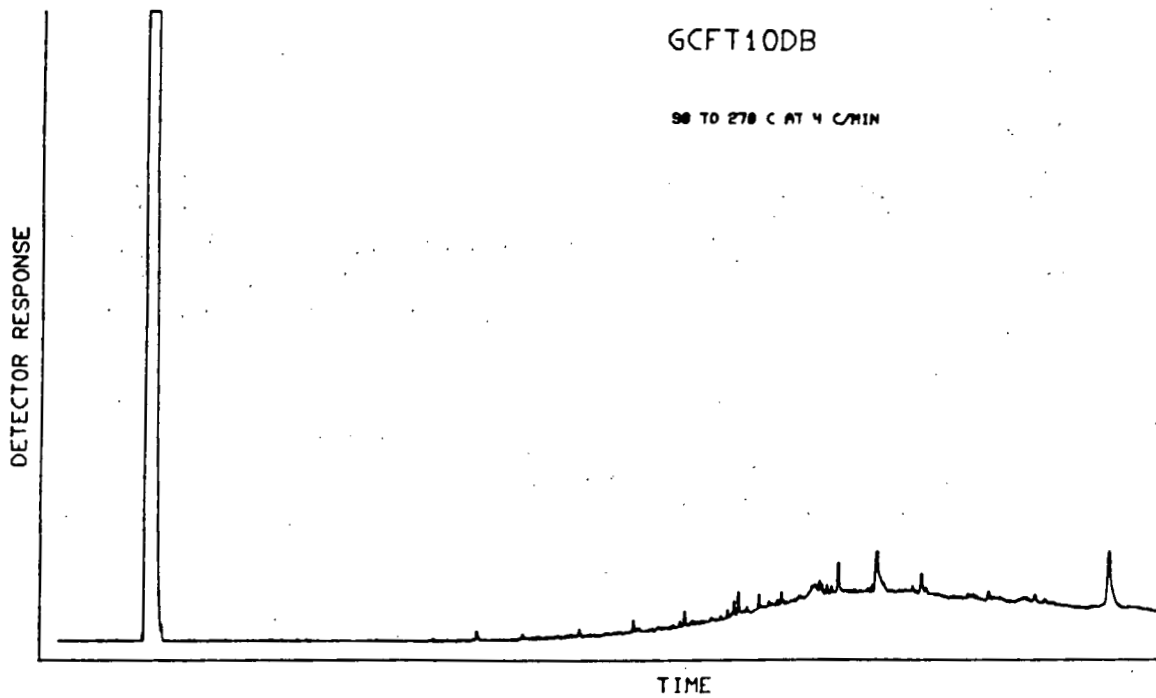


Figure 7.5.11 GC of the Oil/Dispersant Tank, bottom, 1 hr.

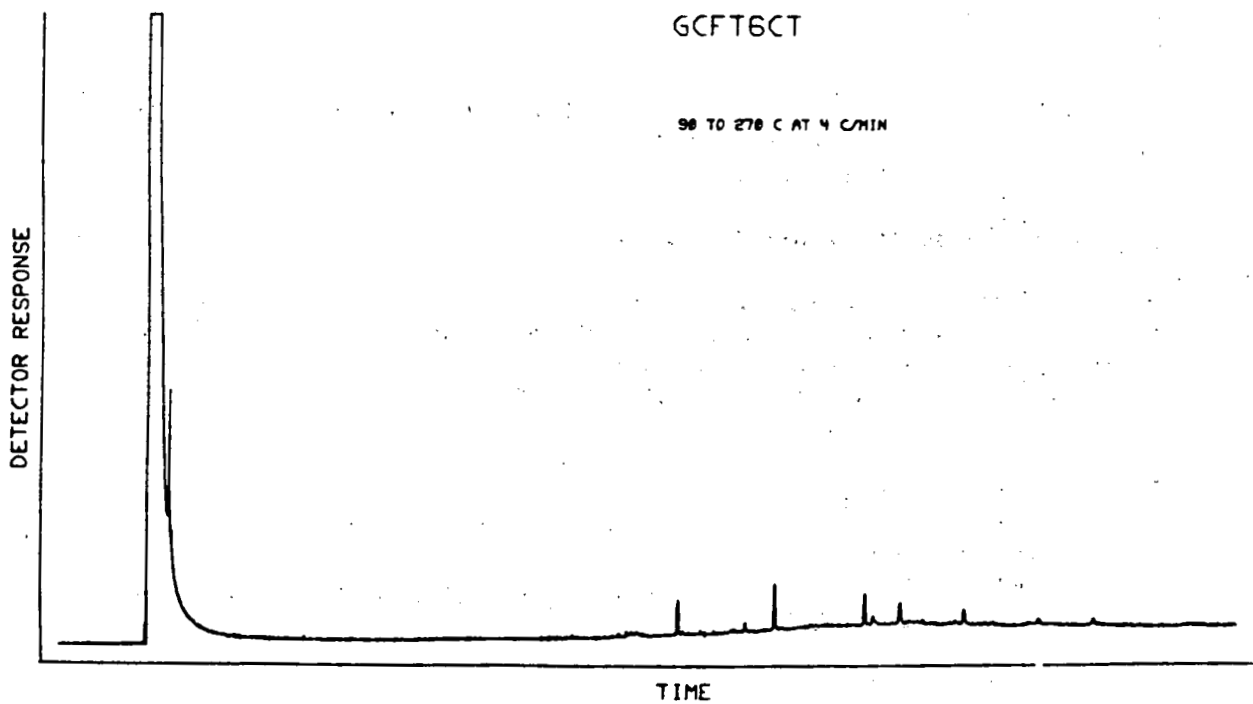


Figure 7.5.12 GC of the Control Tank, top, 6th week.

(b) Week Six

At the beginning of the sixth week, ten ml of dispersant were added to tanks 2, 3 and 4. Water samples were collected for qualitative analysis one hour after the addition of the dispersant.

i. Control Tank

GC of the top, middle and bottom water samples are shown in Figures 7.5.12, 13 and 14. All GC are similar and consist of a series of equally spaced peaks that appear to correspond to the even-numbered normal paraffins. GC of petroleum should consist of a distribution of normal paraffins, whereas biologically produced paraffins are generally odd-numbered.

ii. Dispersant Tank

GC of the top, middle and bottom of the dispersant tank are shown in Figures 7.5.15, 16 and 17. It should be noted that peaks at short retention times are observed after this addition in the top and middle GC, whereas they were not observed after the initial application. The GC of the bottom sample is very similar to that of the controls.

iii. Oil Tank

GC of the top, middle and bottom of the oil tank after dispersant was added, are shown in Figures 7.5.18, 19 and 20. The top and middle are similar, consisting of a number of peaks due to the dispersant. None of the peaks can be definitely assigned to the oil. With the exception of one strong peak, the GC of the bottom is similar to those of the controls.

iv. Oil/Dispersant Tank

GC of the top, middle and bottom samples are shown in Figures 7.5.21, 22 and 23. All three GCs correspond closely to those of the dispersant and oil tanks at the same levels.

(B) Fractionation of Water Extracts

Extracts of the top samples from tanks 1, 3 and 4 collected at the first hour were separated by a liquid column into 7 to 8 fractions. The GC of fractions from the control tank are shown in Figures 7.5.24 to 30. The heavier normal paraffins are observed in fractions 1, 2 and 3; whereas light components (shorter retention times) are observed in 4 thru 7. GC of the fractions from the top of the oil tank are shown in Figures 7.5.31 to 38. In this sequence, paraffins should appear in the first fraction, followed by one ring aromatics, two ring aromatics, multi-ring aromatics, and polar compounds. Fraction 3 (Figure 7.5.33) presents the most interesting GC; the peaks are possibly due to substituted two or three ring aromatics.

Due to the higher concentrations in the oil/dispersant tank, fractionation of this sample produced the strongest GC's as are shown in Figures 7.5.39-46. In the GC of the first fraction, paraffins, both normal and isoprenoids, are clearly separated into individual peaks.

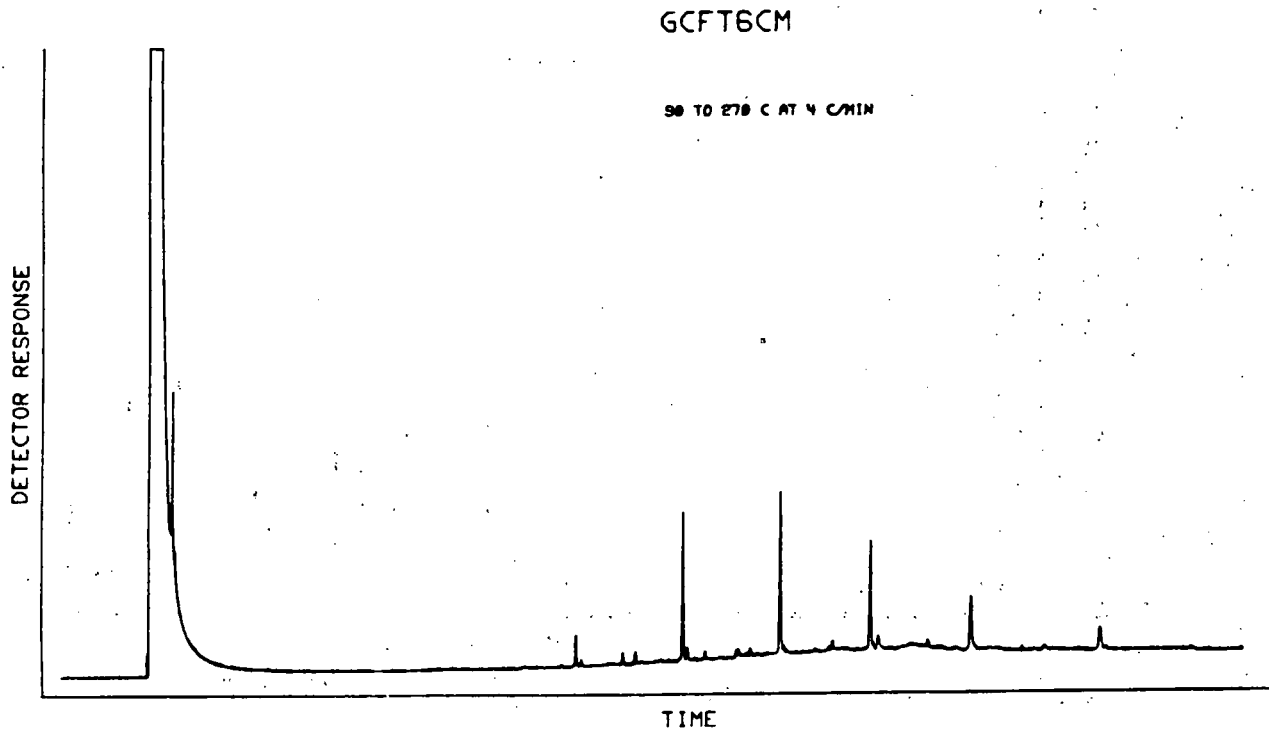


Figure 7.5.13 GC of the Control Tank, middle, 6th week.

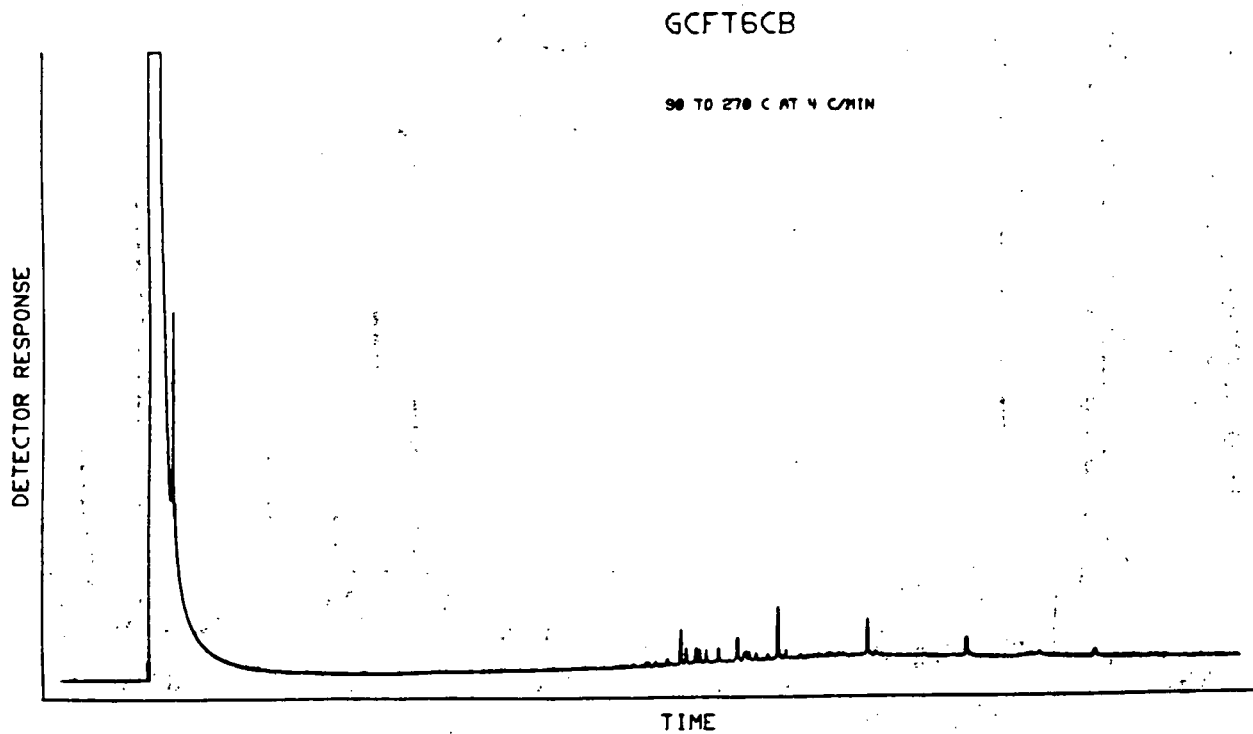


Figure 7.5.14 GC of the Control Tank, bottom, 6th week.

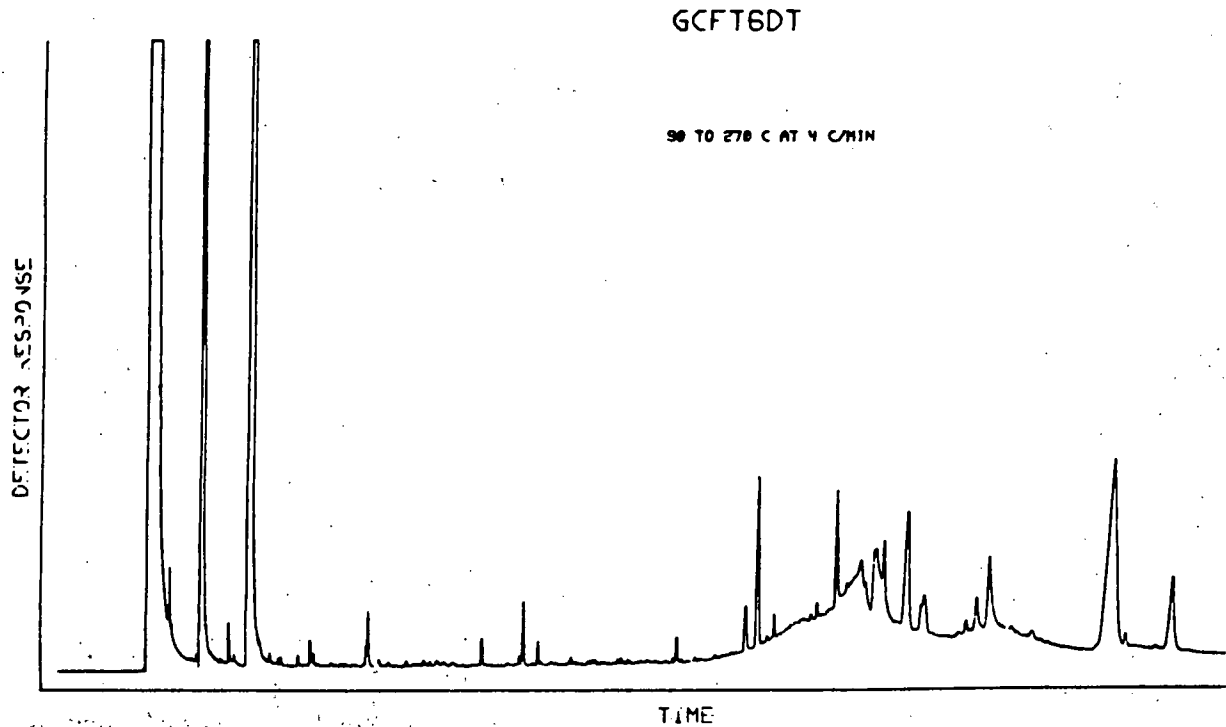


Figure 7.5.15 GC of the Dispersant Tank, top, 6th week.

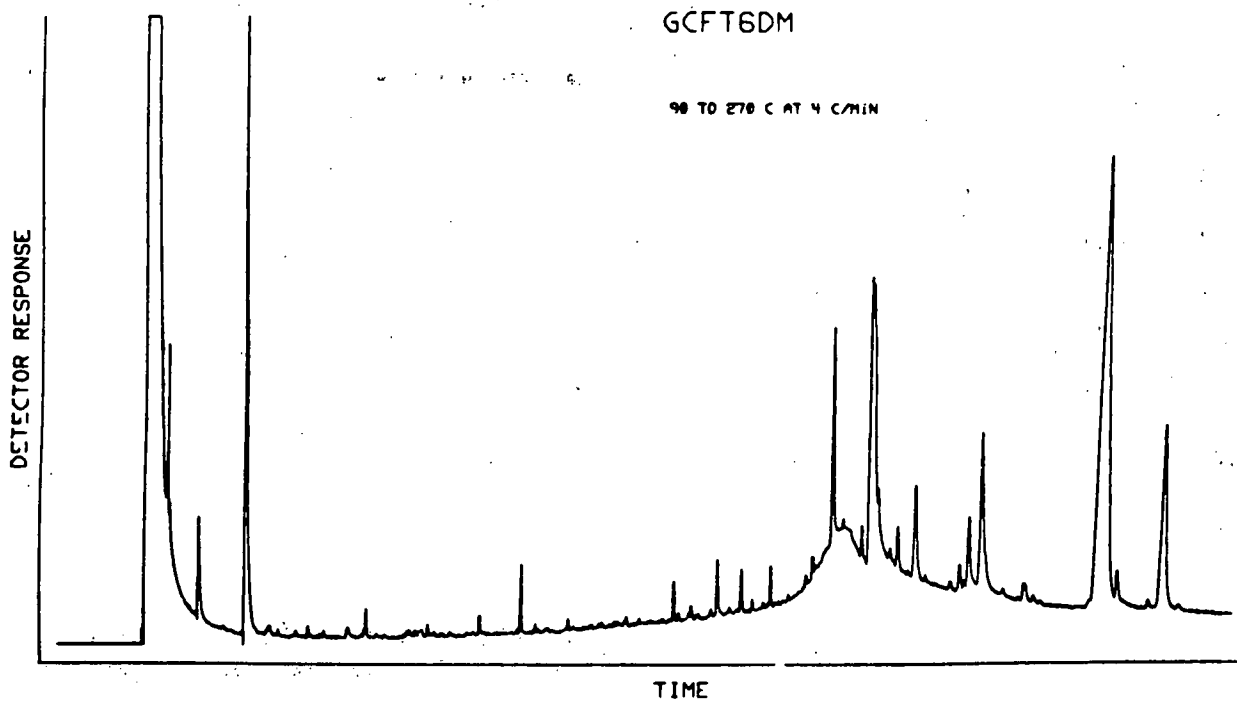


Figure 7.5.16 GC of the Dispersant Tank, middle, 6th week.

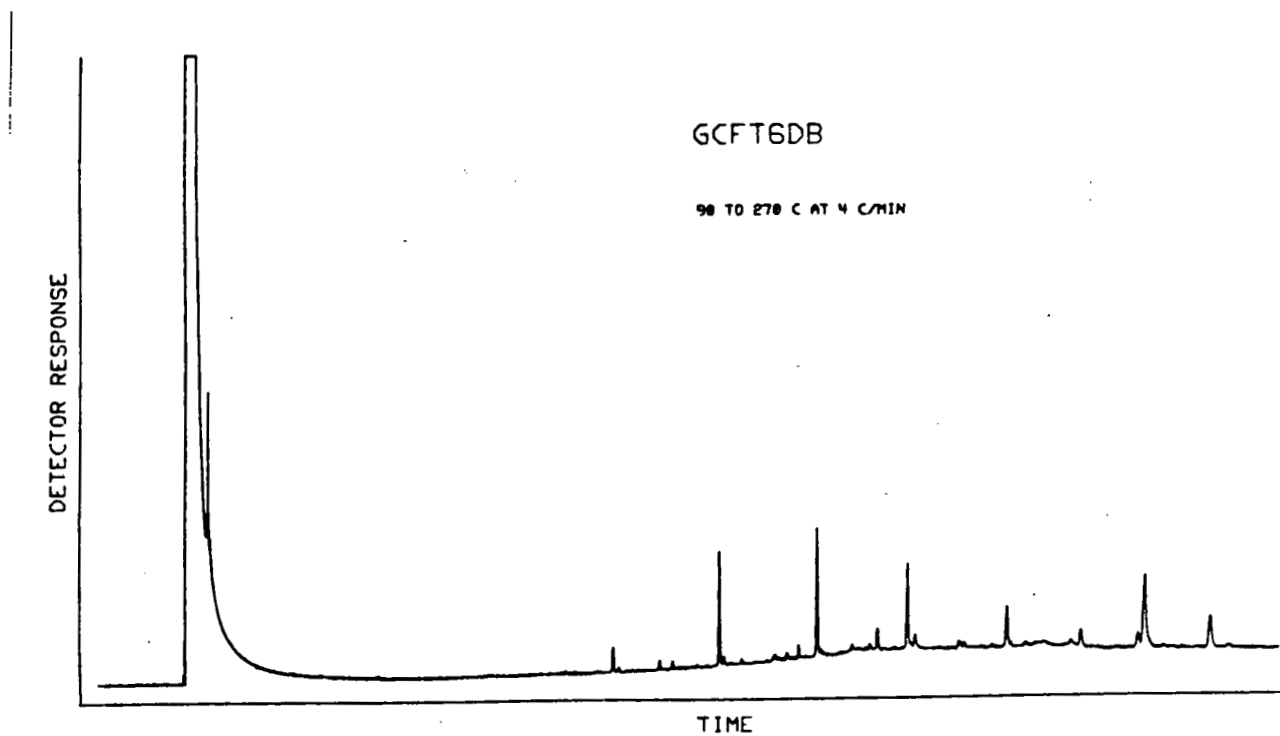


Figure 7.5.17 GC of the Dispersant Tank, bottom, 6th week.

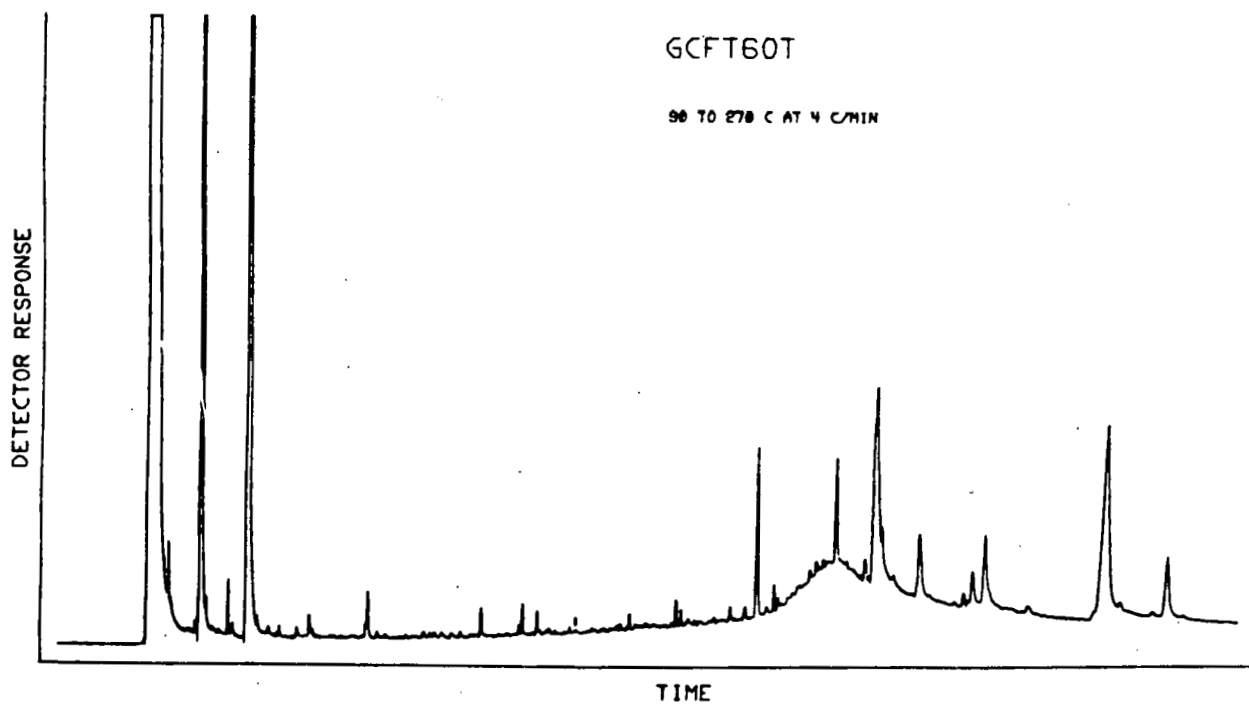


Figure 7.5.18 GC of the Oil Tank, top, 6th week.

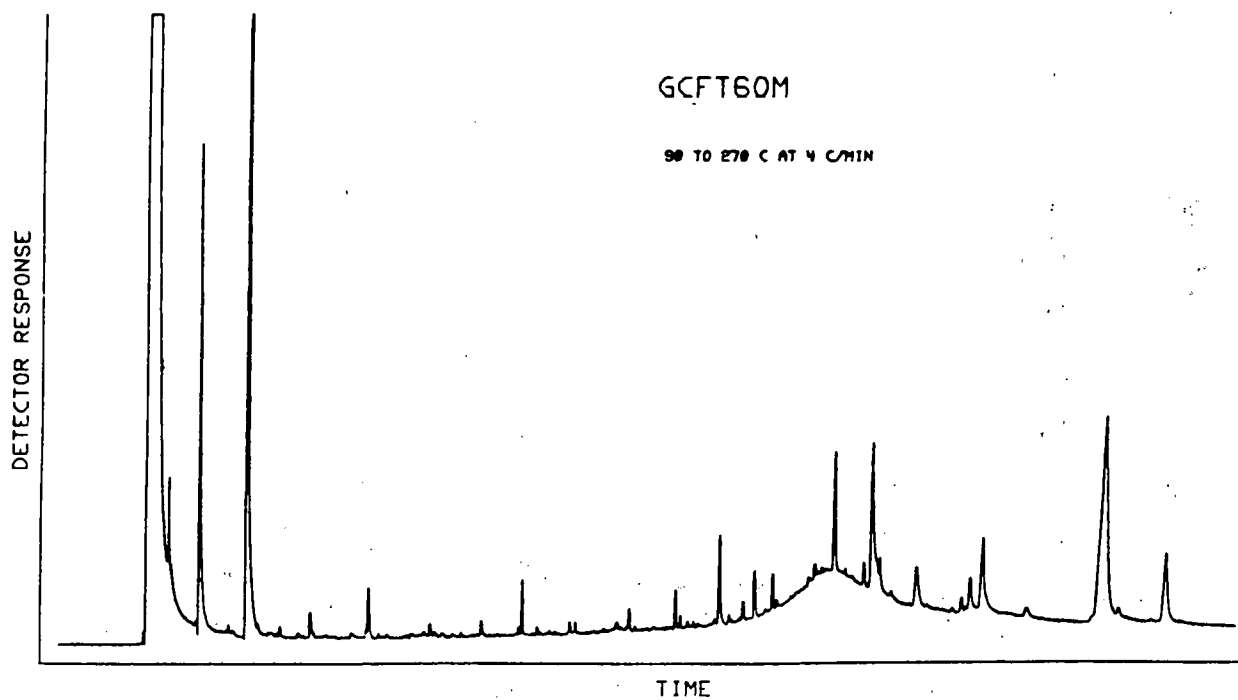


Figure 7.5.19 GC of the Oil Tank, middle, 6th week.

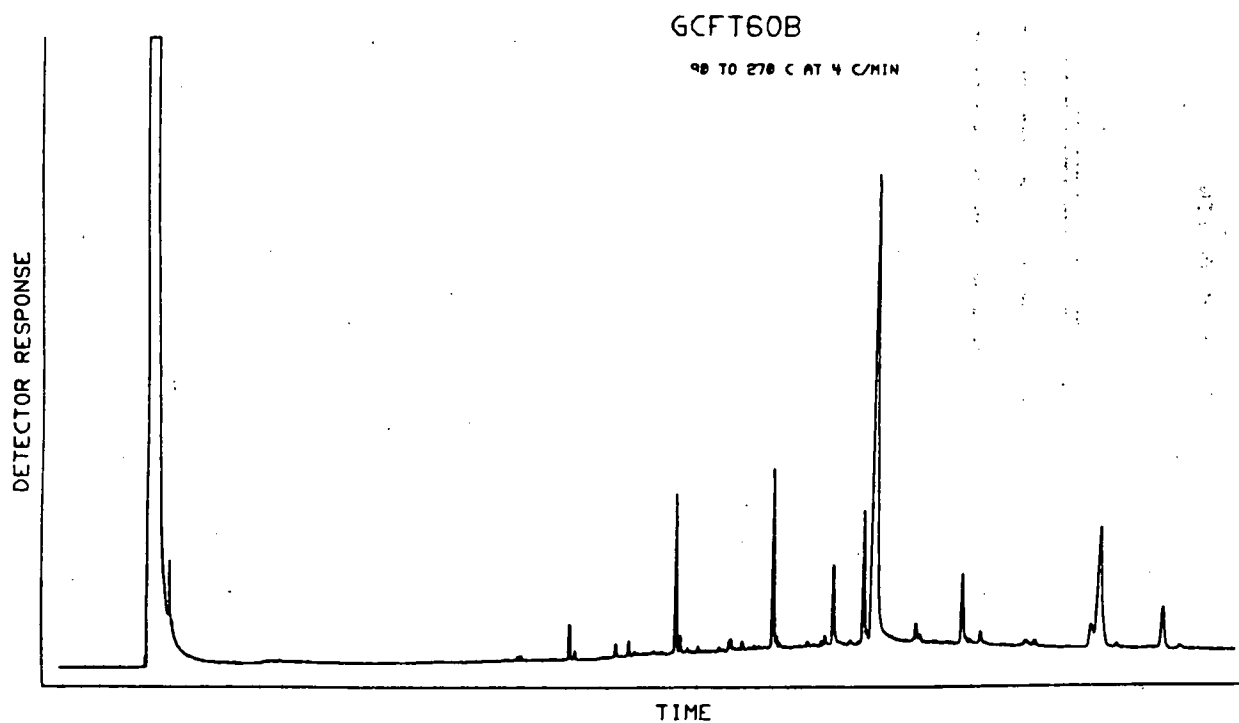


Figure 7.5.20 GC of the Oil Tank, bottom, 6th week.

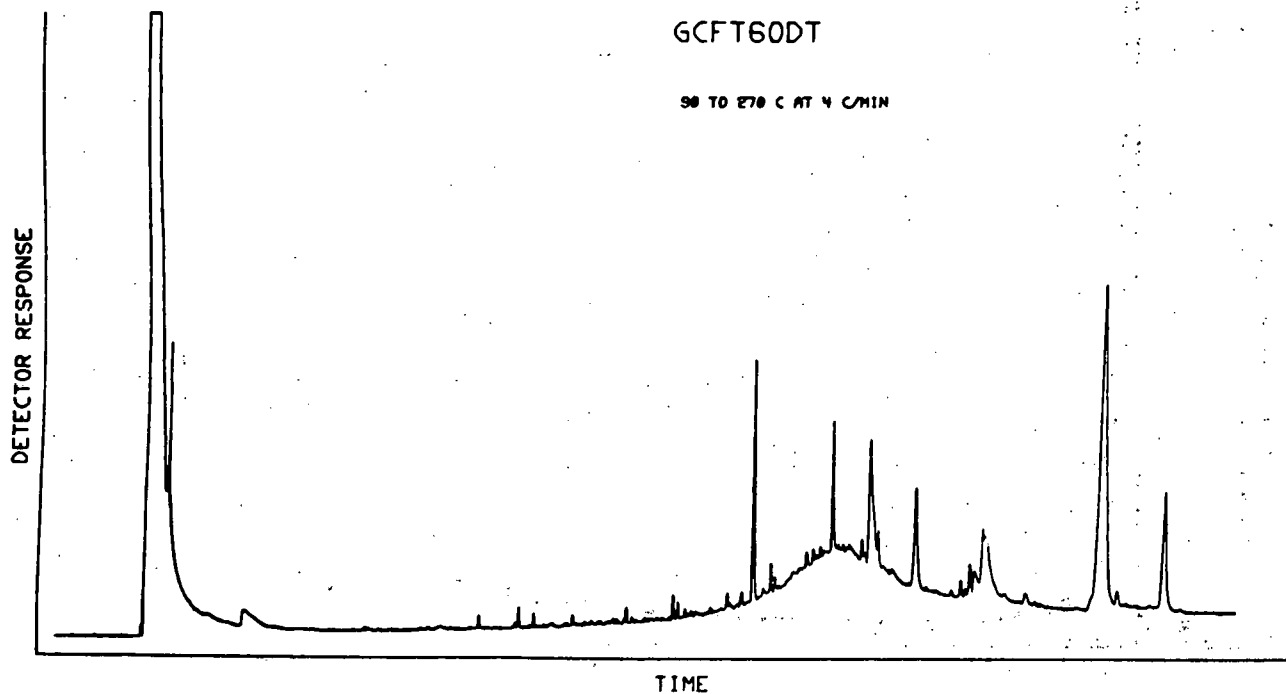


Figure 7.5.21 GC of the Oil/Dispersant Tank, top, 6th week.

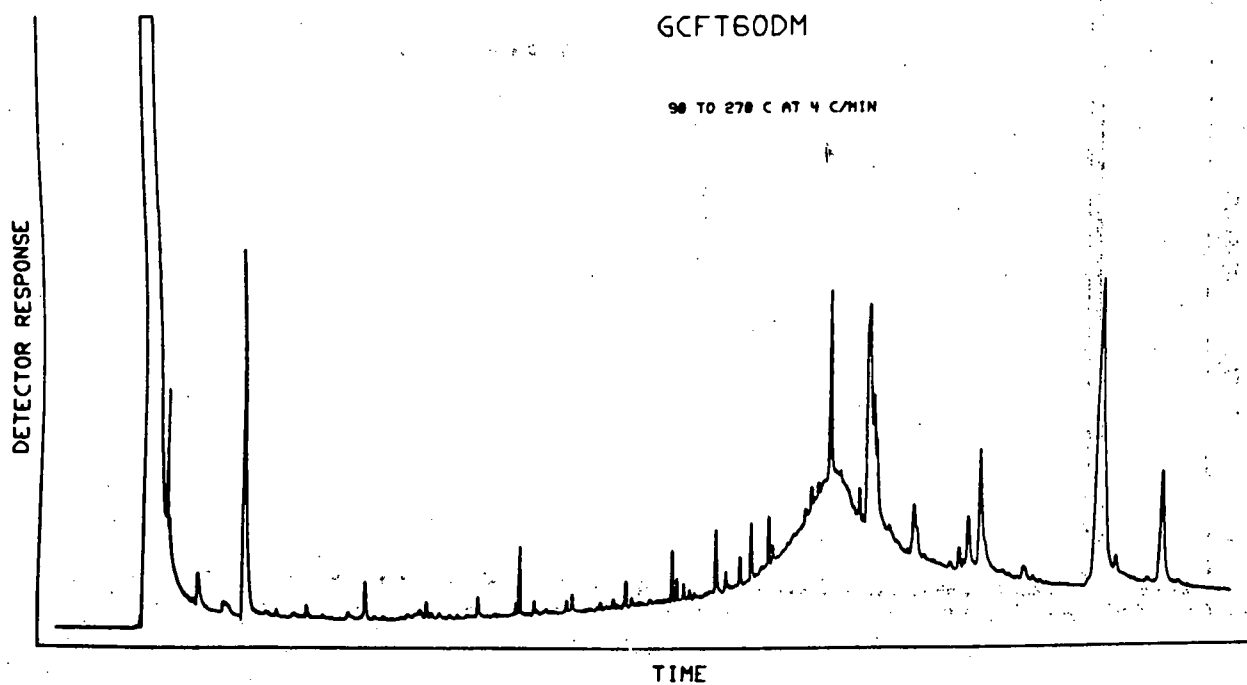


Figure 7.5.22 GC of the Oil/Dispersant Tank, middle, 6th week.

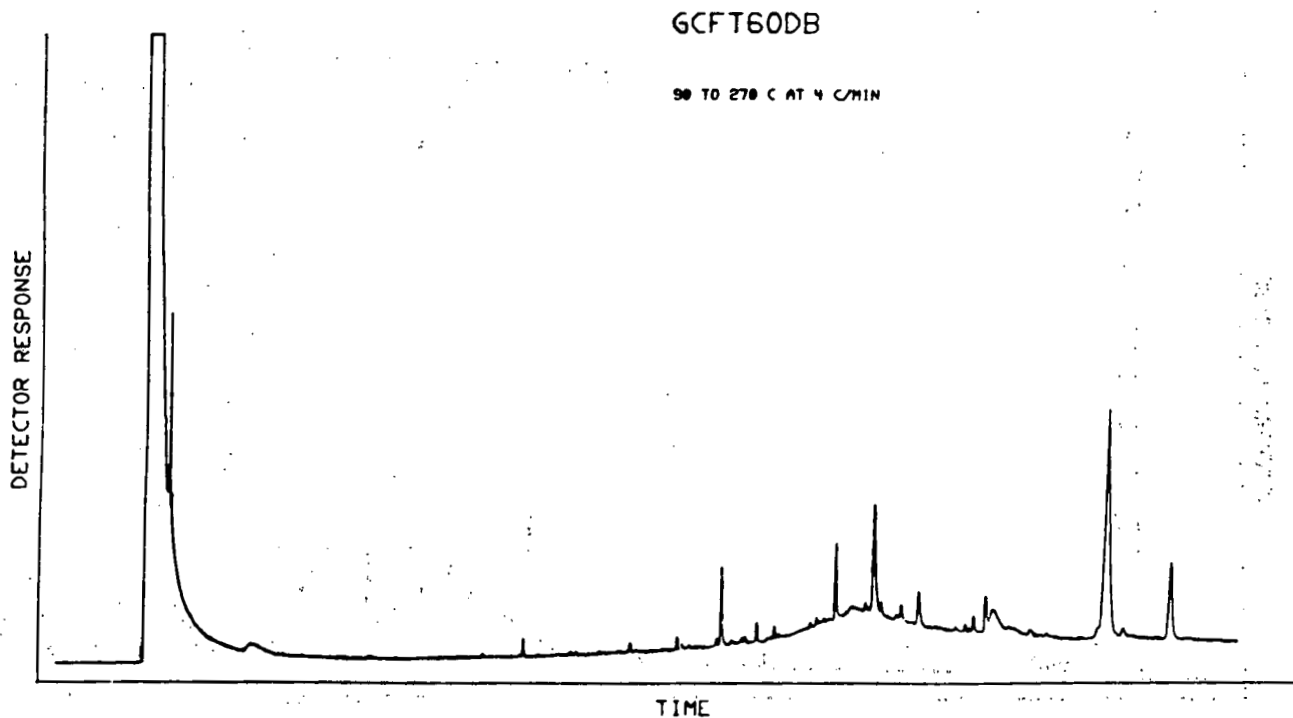


Figure 7.5.23 GC of the Oil/Dispersant Tank, bottom, 6th week.

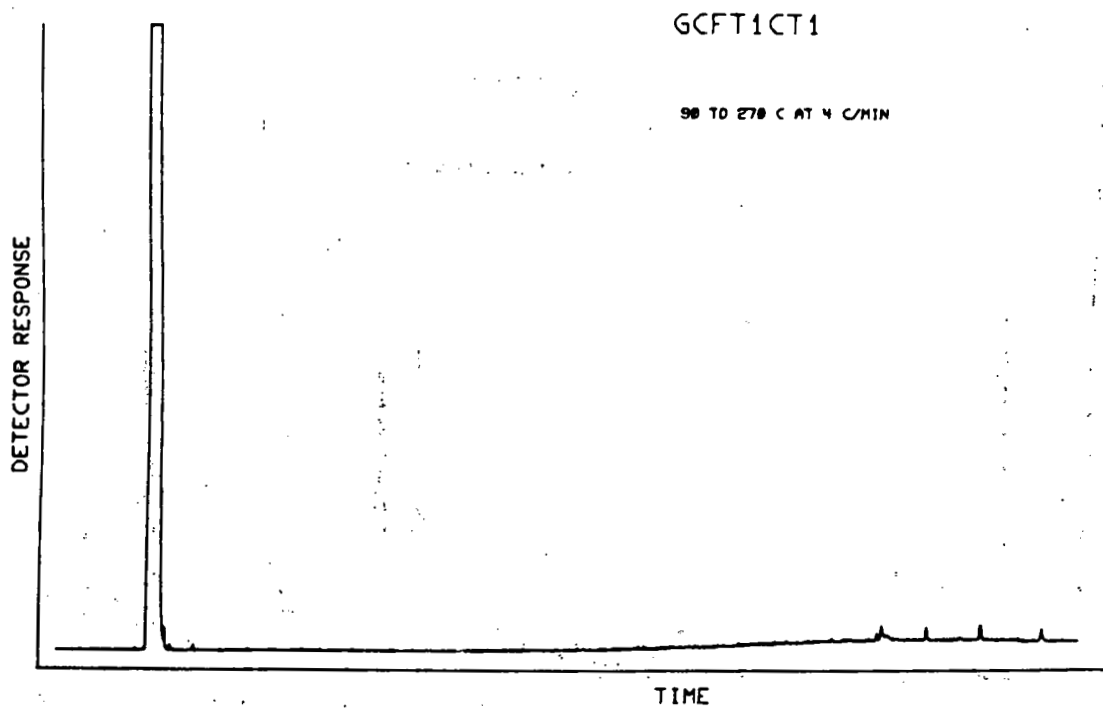


Figure 7.5.24 GC of the Control Tank, top, 1 hr, fraction 1.

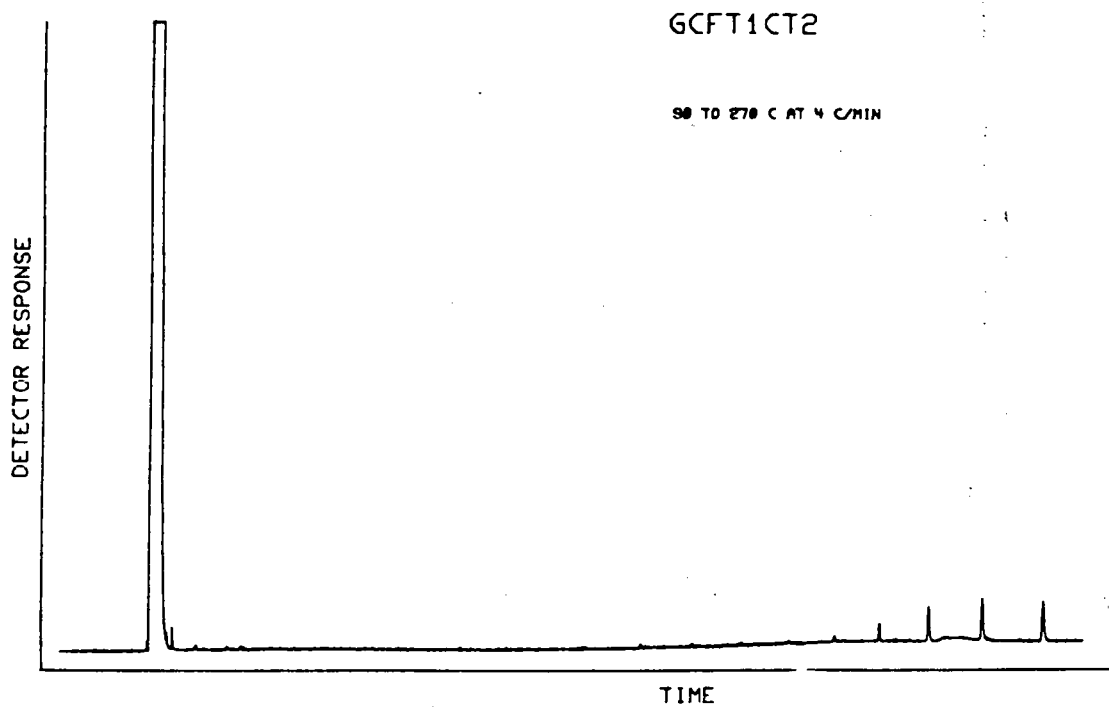


Figure 7.5.25 GC of the Control Tank, top, 1 hr, fraction 2.

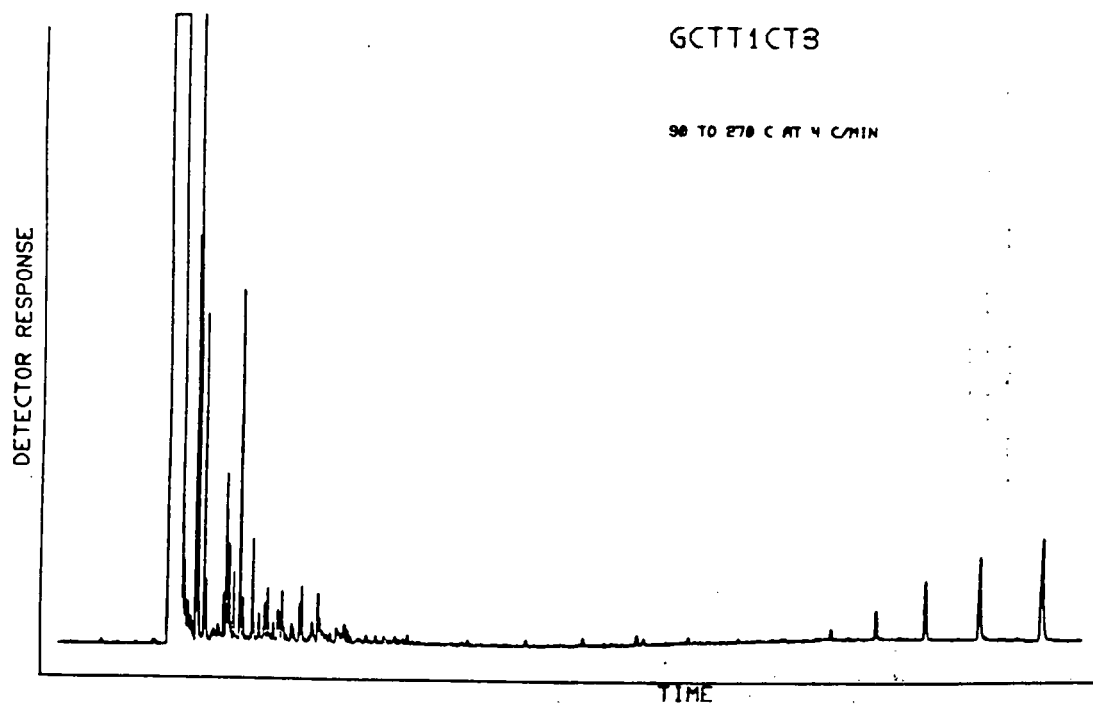


Figure 7.5.26 GC of the Control Tank, top, 1 hr, fraction 3.

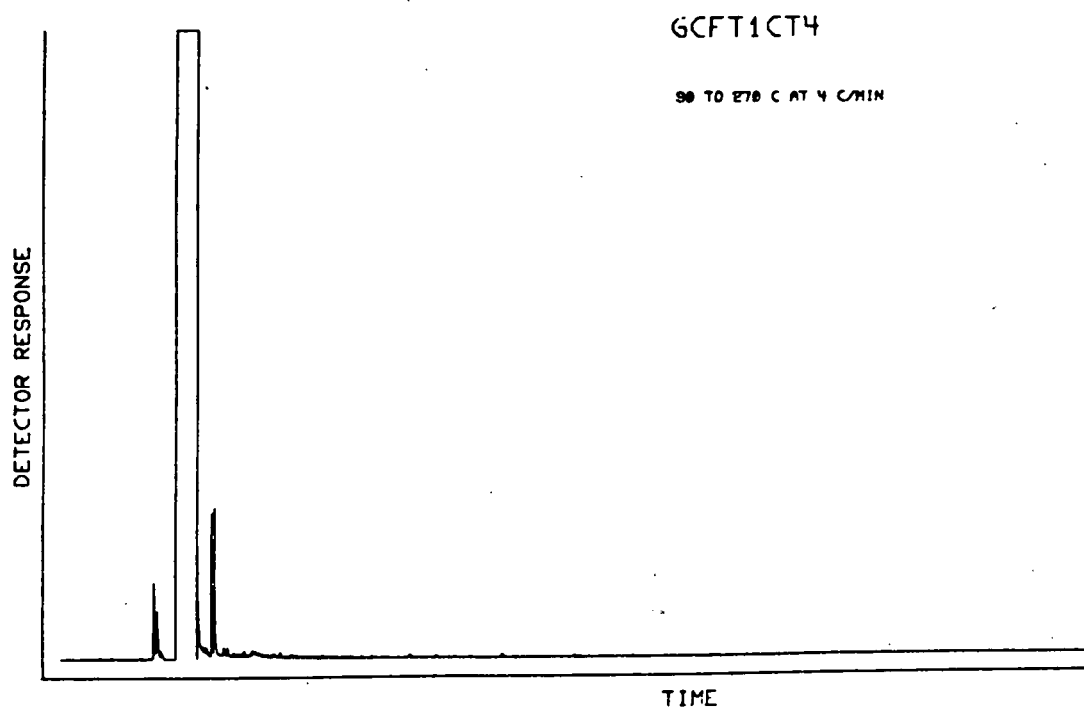


Figure 7.5.27 GC of the Control Tank, top, 1 hr, fraction 4.

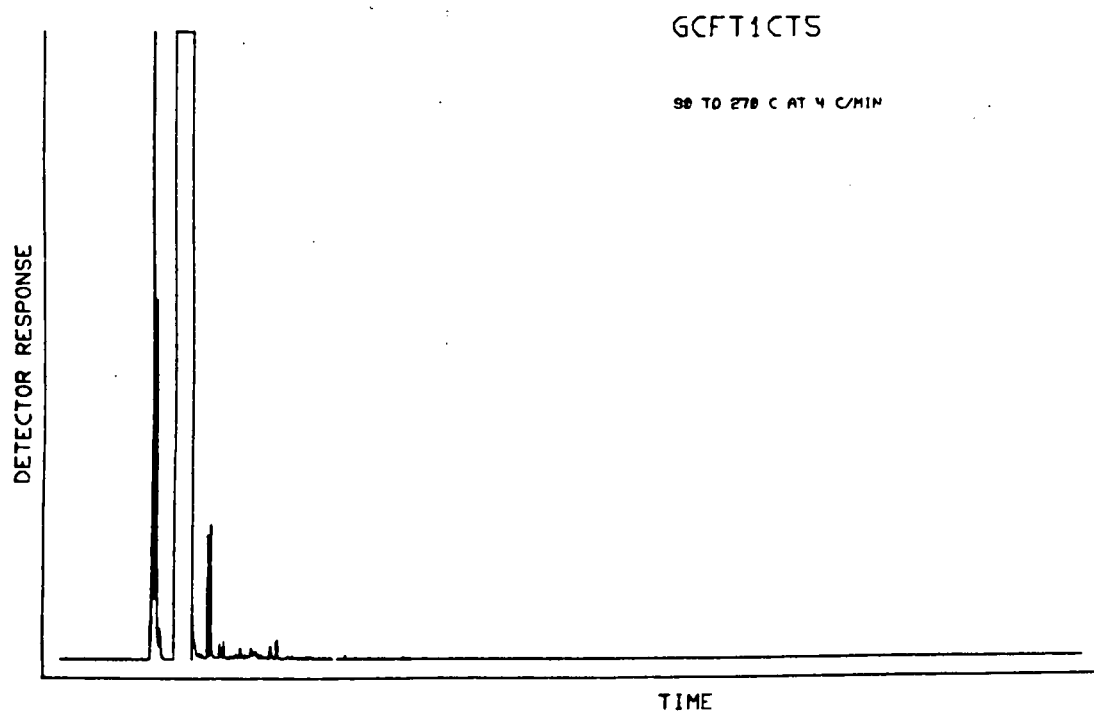


Figure 7.5.28 GC of the Control Tank, top, 1 hr, fraction 5.

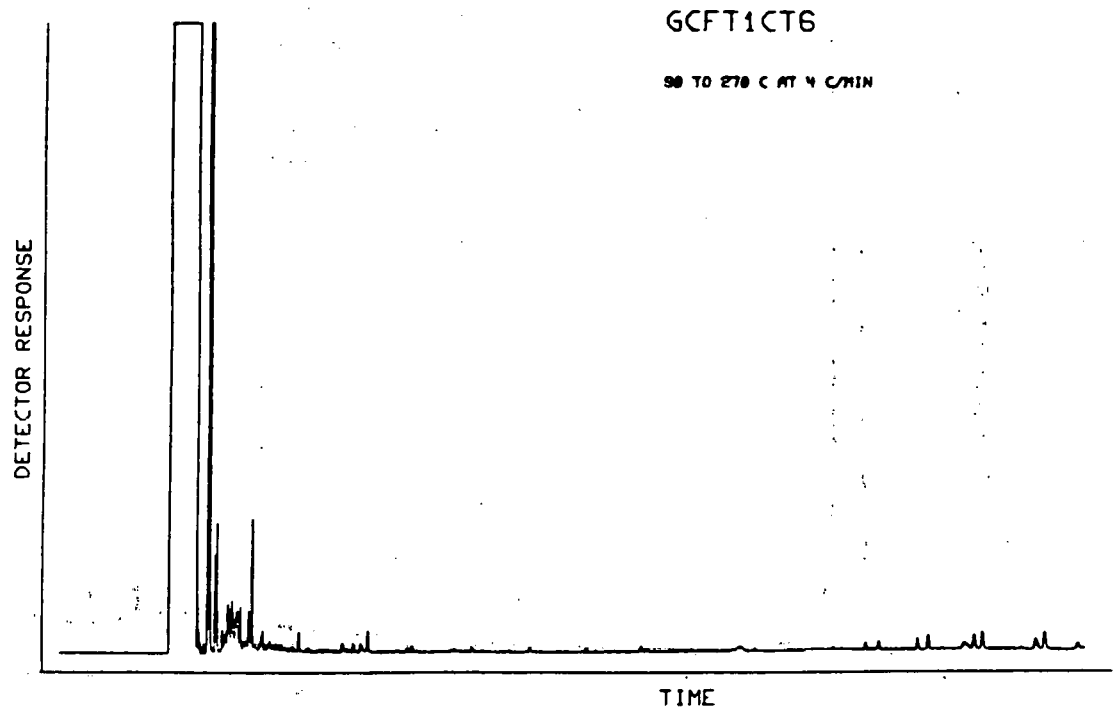


Figure 7.5.29 GC of the Control Tank, top, 1 hr, fraction 6.

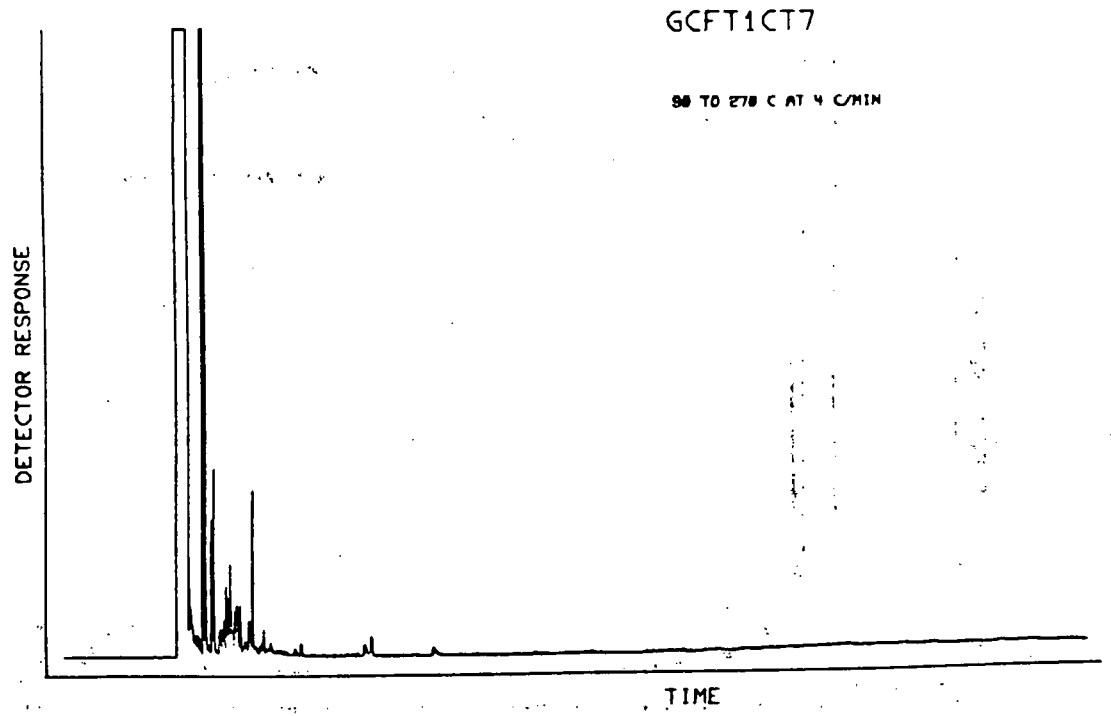


Figure 7.5.30 GC of the Control Tank, top, 1 hr, fraction 7.

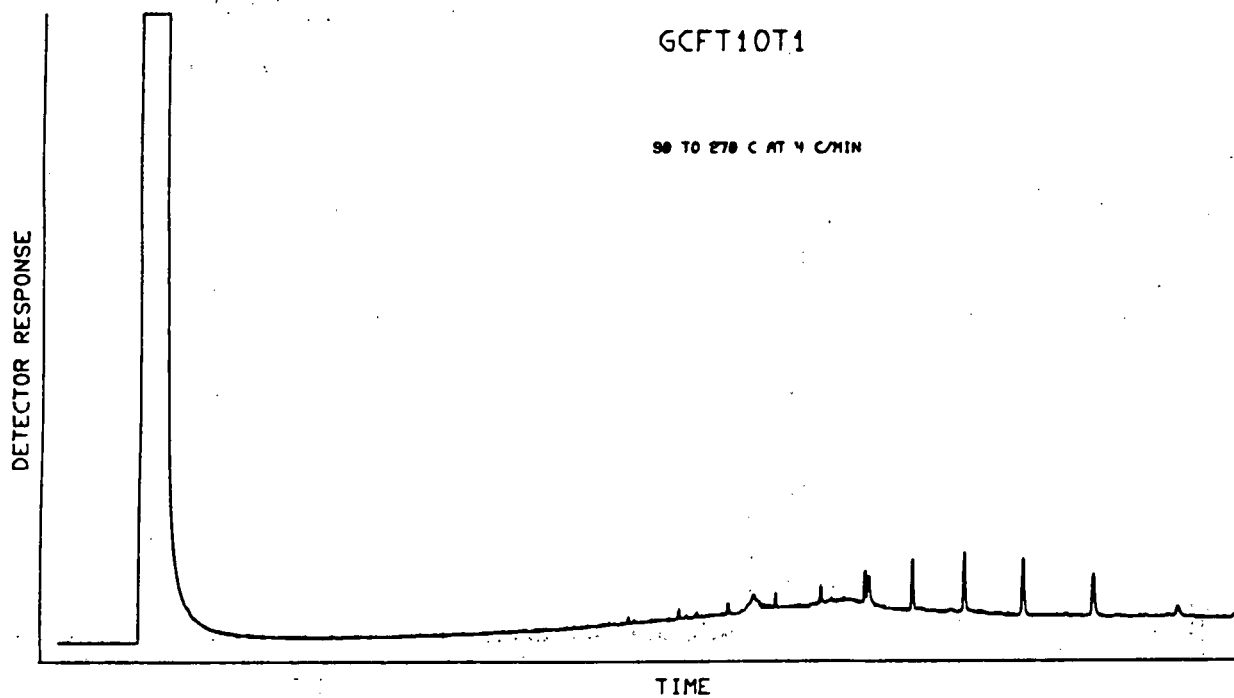


Figure 7.5.31 GC of the Oil Tank, top, 1 hr, fraction 1.

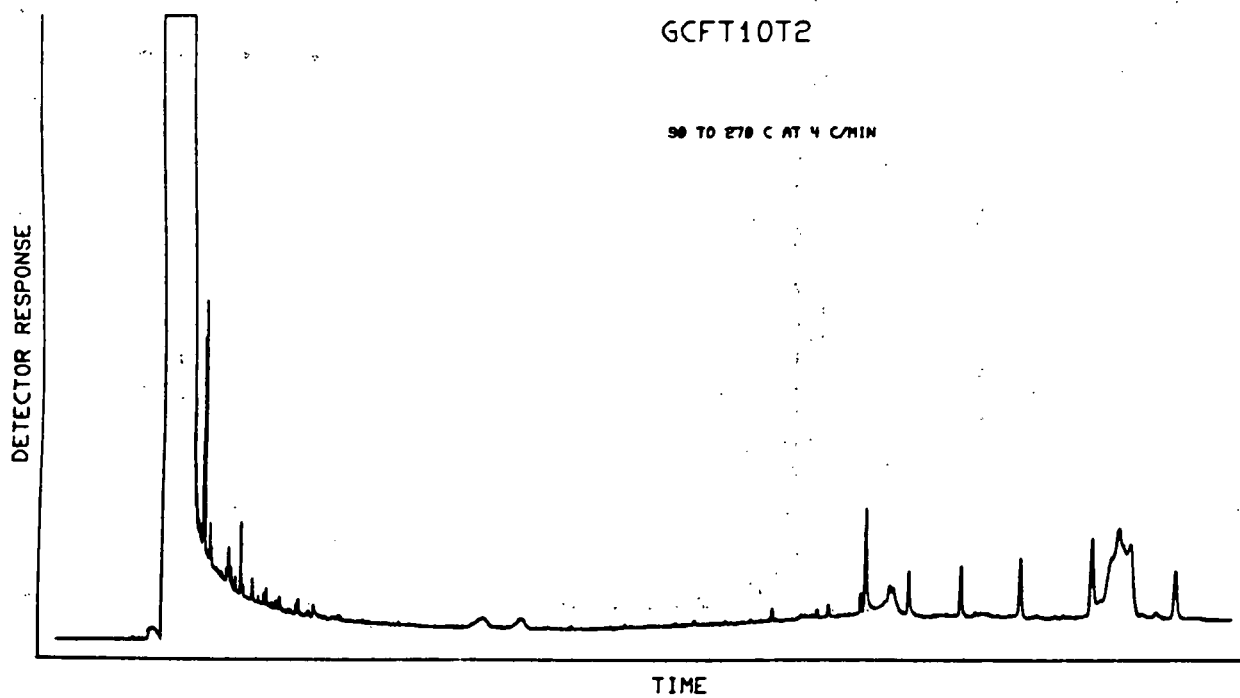


Figure 7.5.32 GC of the Oil Tank, top, 1 hr, fraction 2.

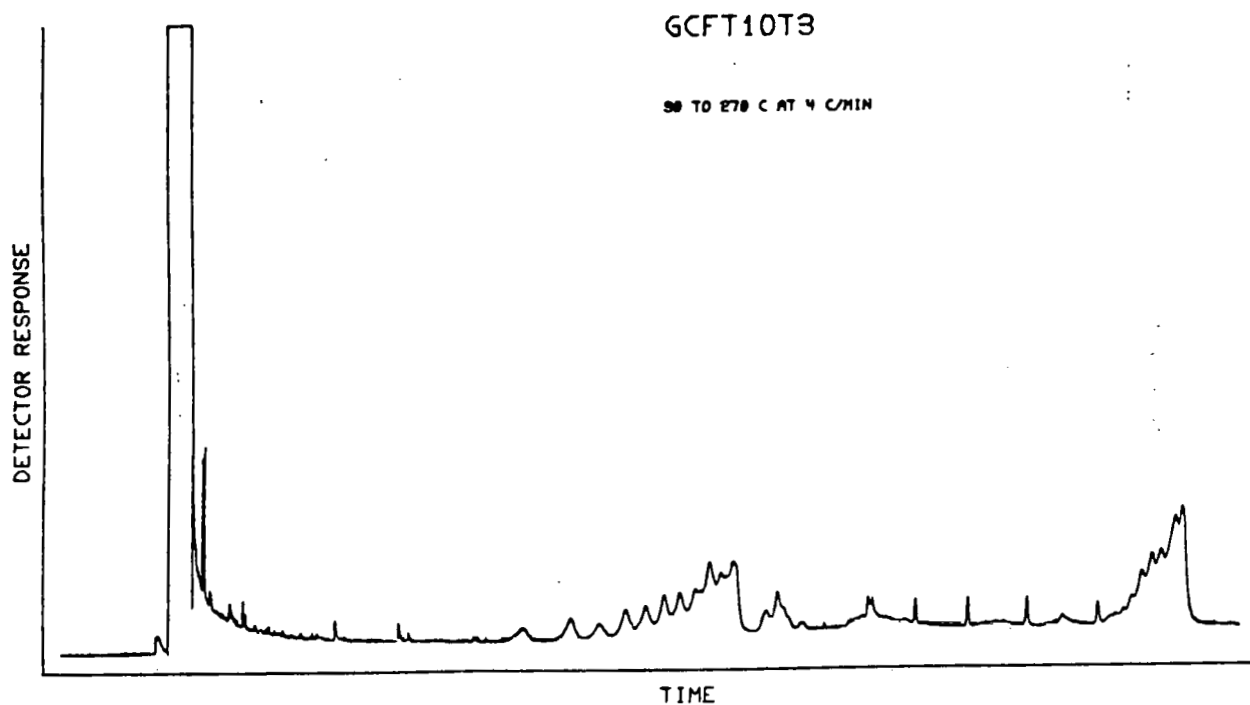


Figure 7.5.33 GC of the Oil Tank, top, 1 hr, fraction 3.

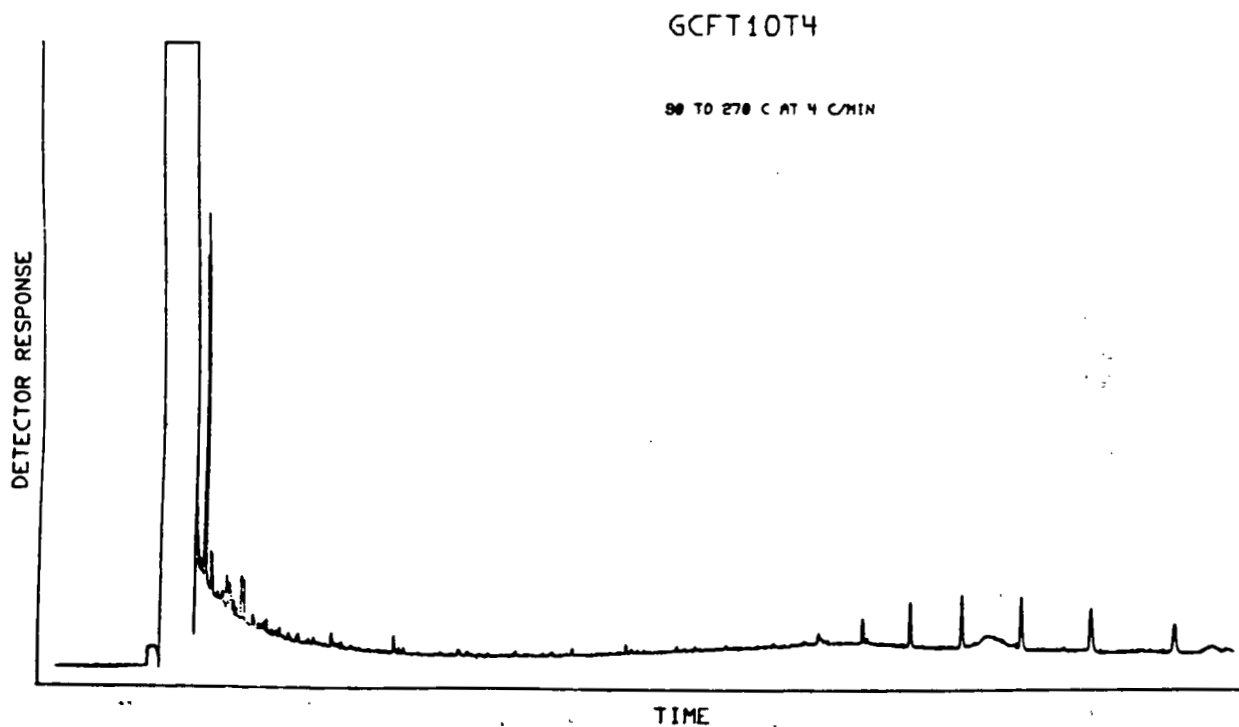


Figure 7.5.34 GC of the Oil Tank, top, 1 hr, fraction 4.

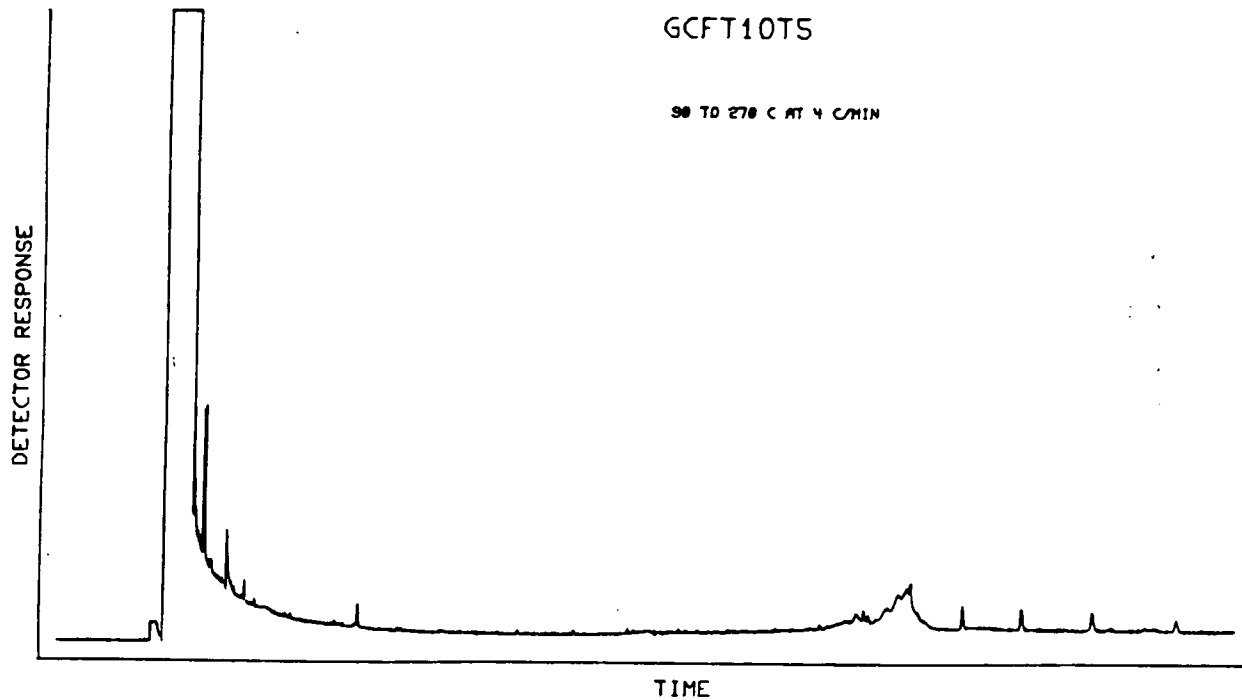


Figure 7.5.35 GC of the Oil Tank, top, 1 hr, fraction 5.

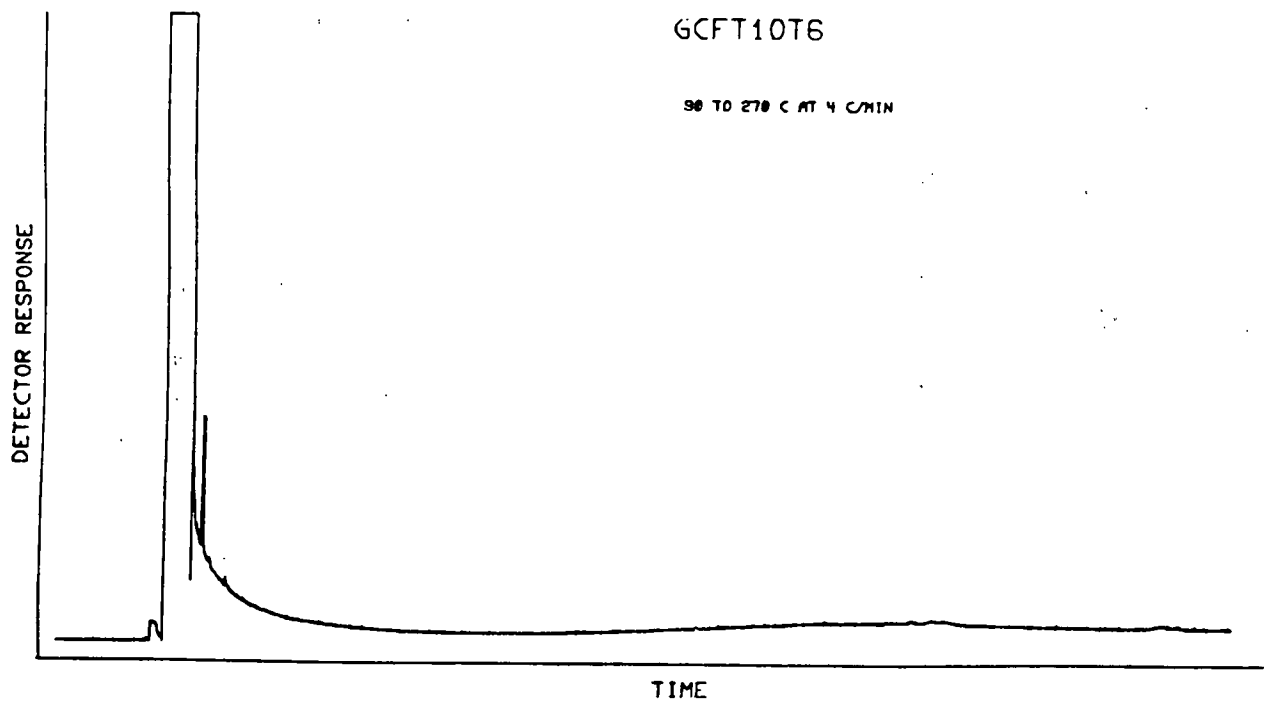


Figure 7.5.36 GC of the Oil Tank, top, 1 hr, fraction 6.

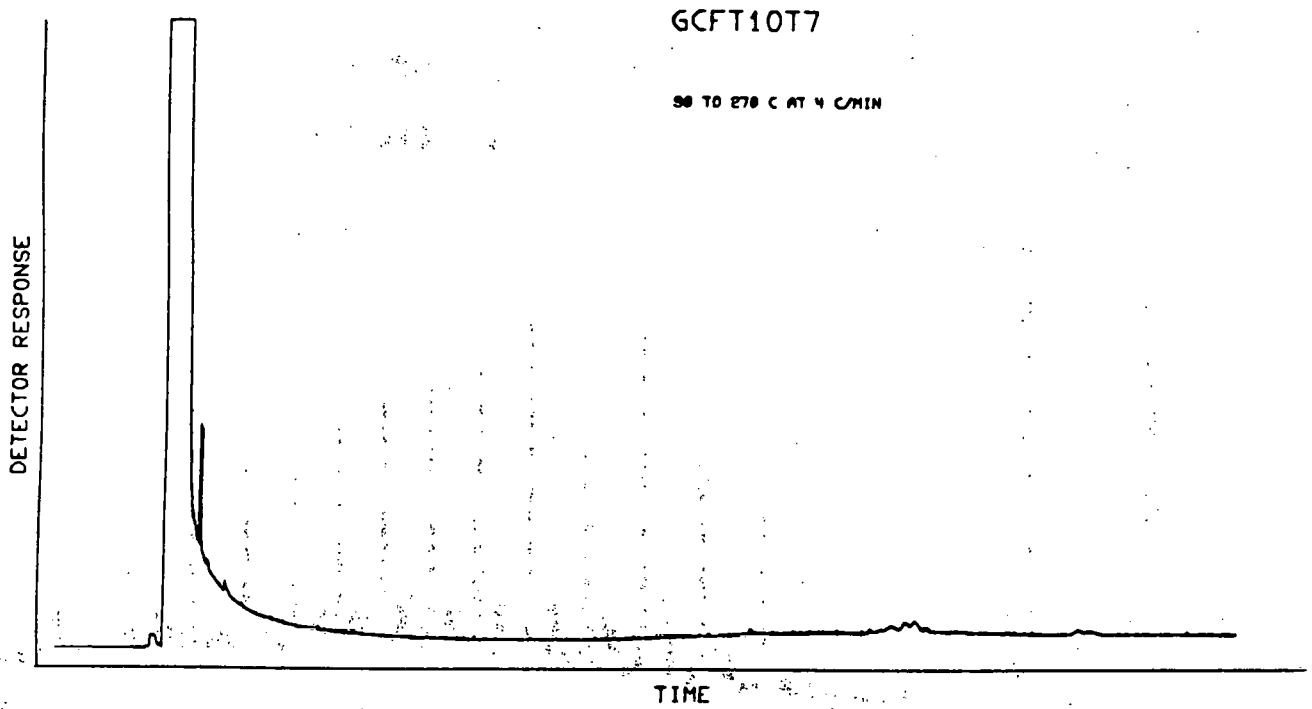


Figure 7.5.37 GC of the Oil Tank, top, 1 hr., fraction 7.

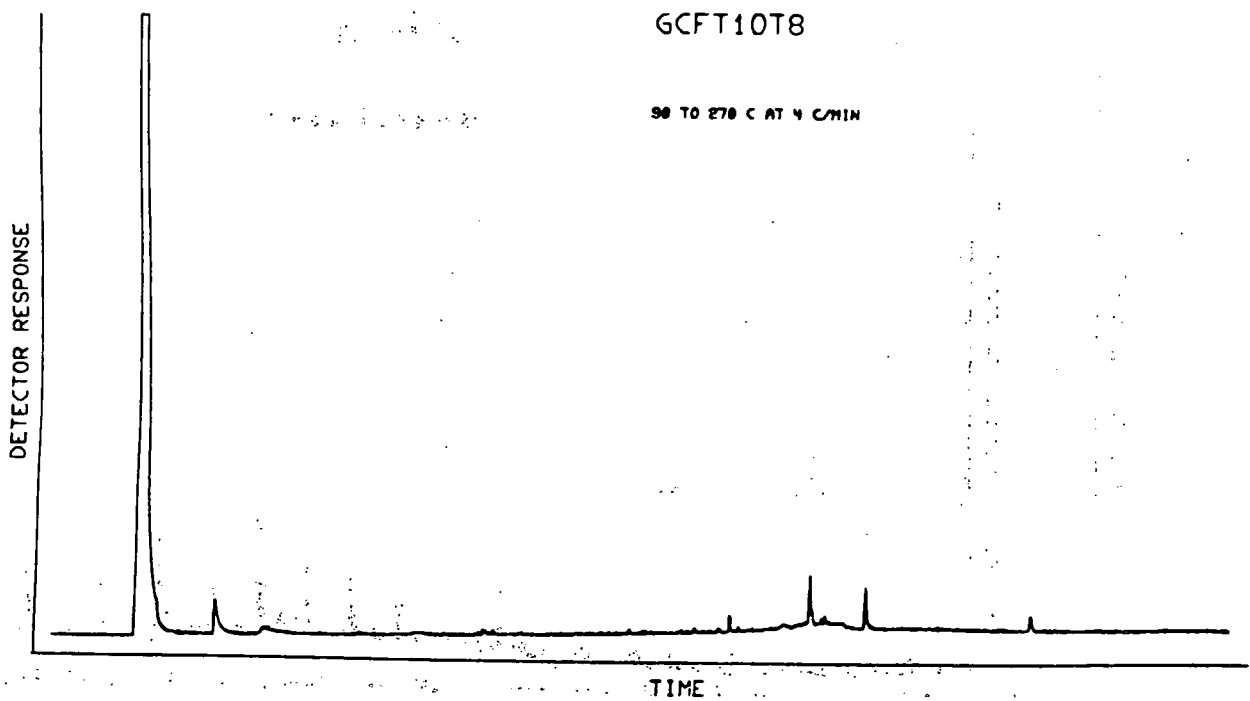


Figure 7.5.38 GC of the Oil Tank, top, 1 hr, fraction 8.

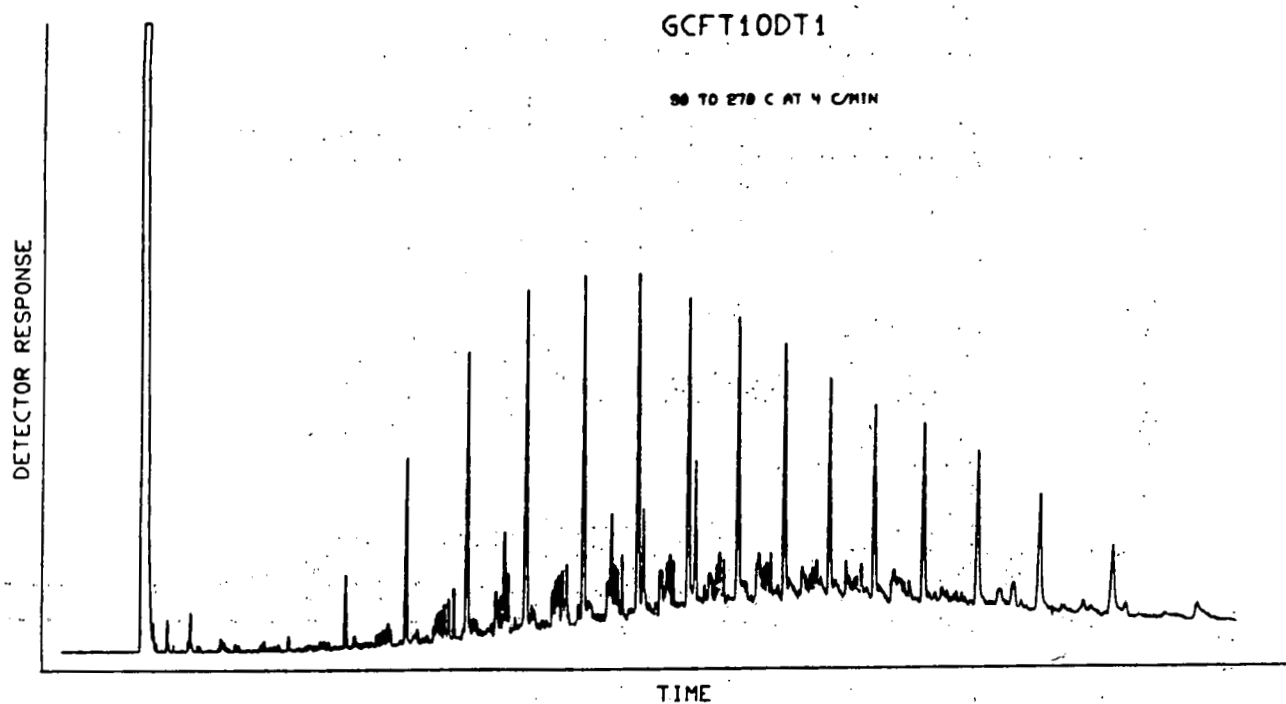


Figure 7.5.39 GC of the Oil/Dispersant Tank, 1 hr, fraction 1.

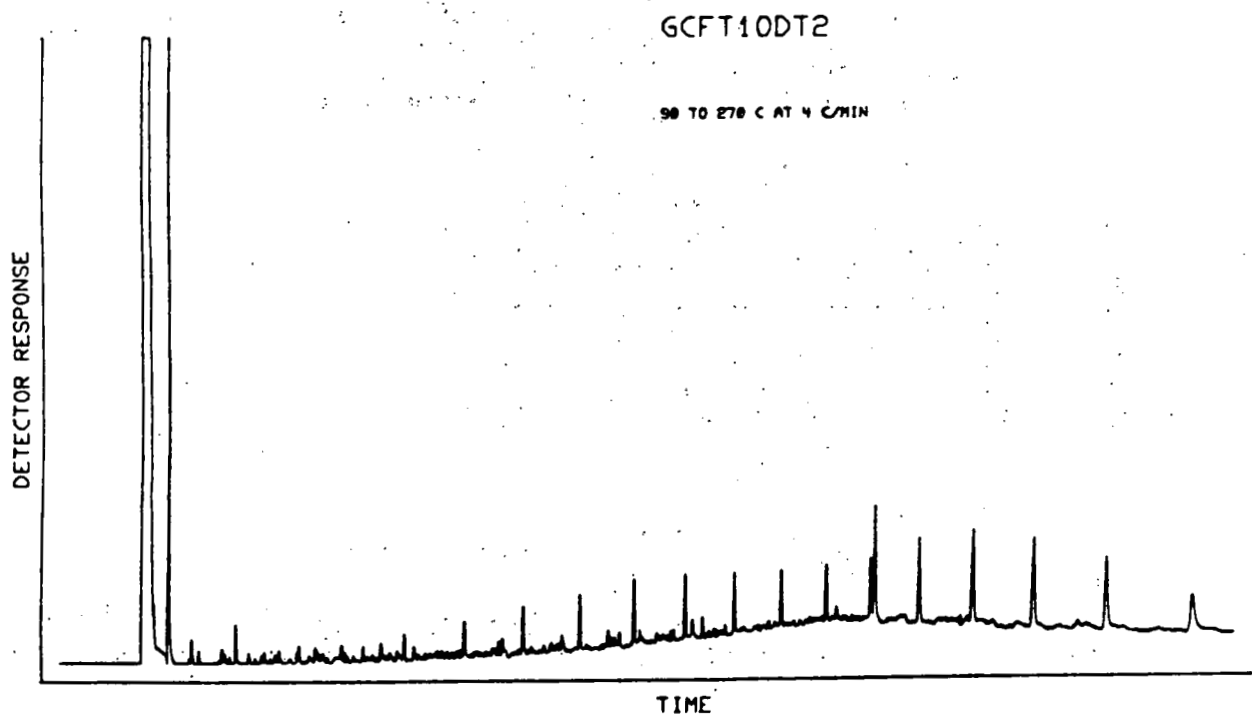


Figure 7.5.40 GC of the Oil/Dispersant Tank, 1 hr, fraction 2.

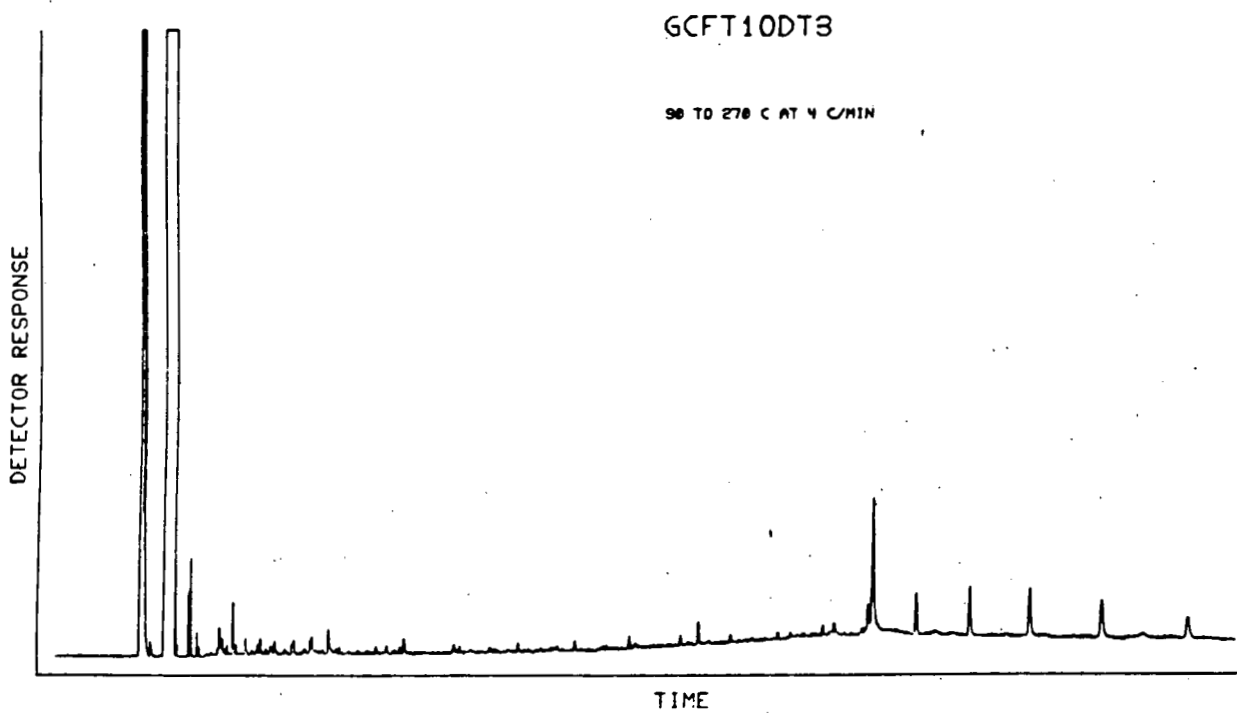


Figure 7.5.41 GC of the Oil/Dispersant Tank, 1 hr, fraction 3.

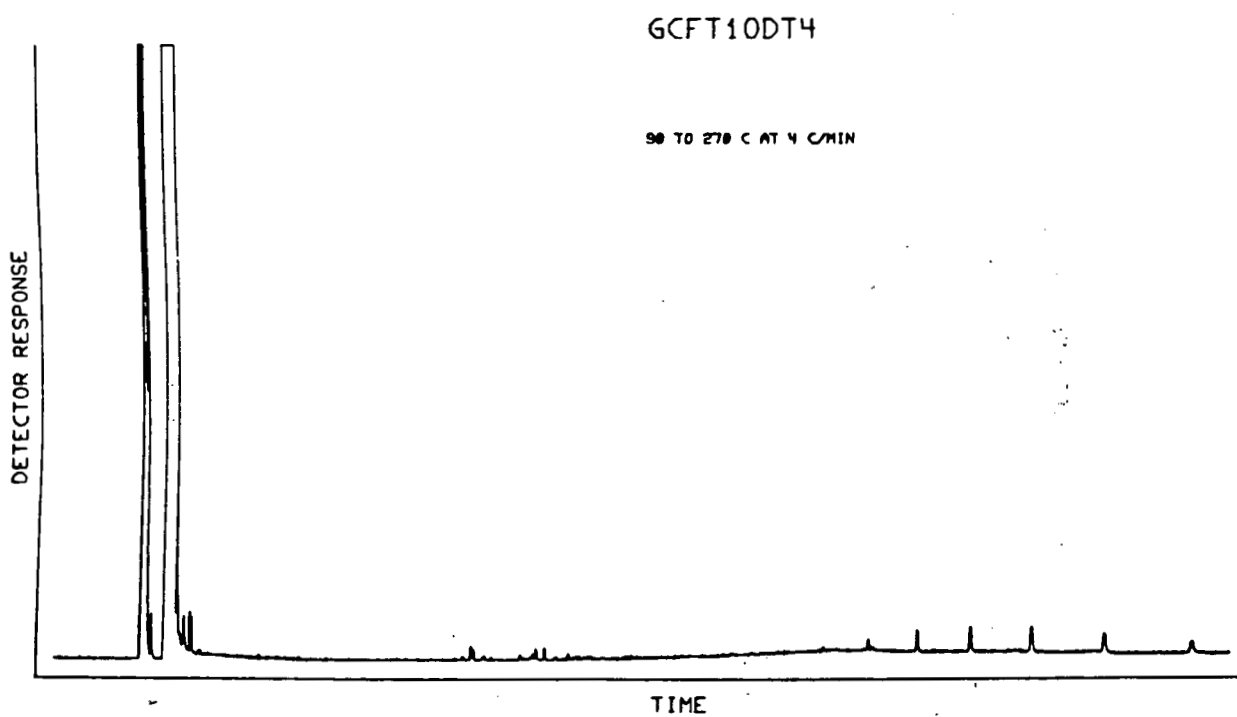


Figure 7.5.42 GC of the Oil/Dispersant Tank, 1 hr, fraction 4.

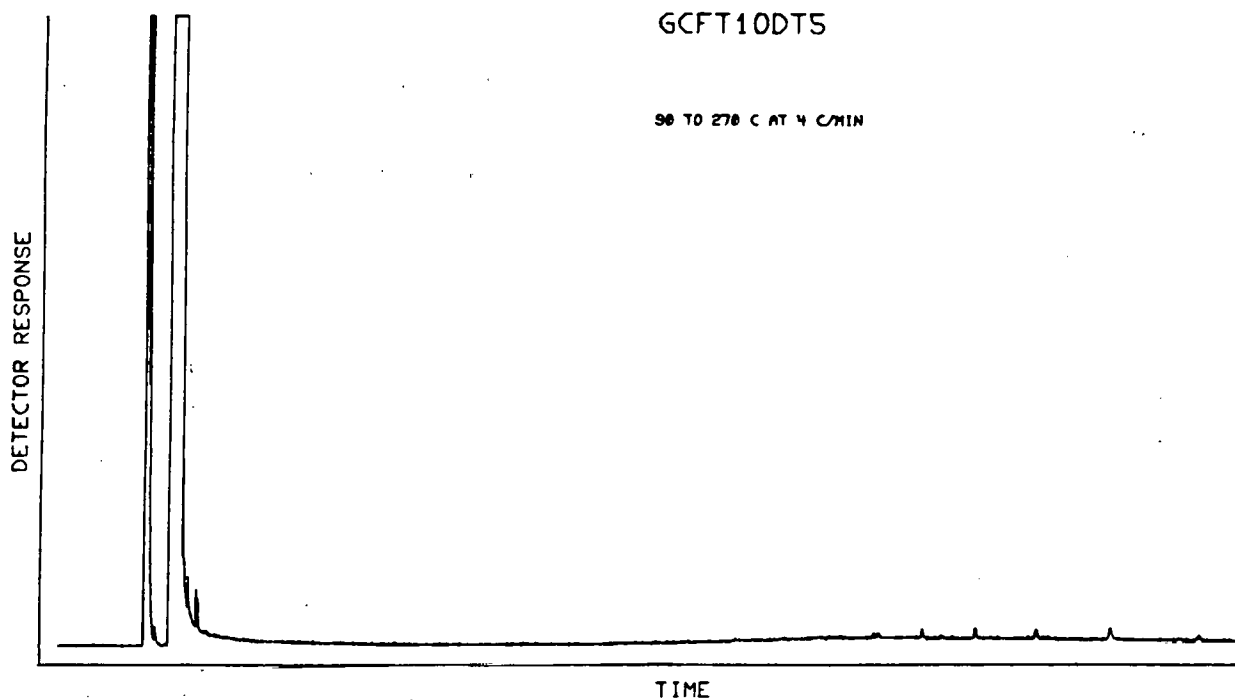


Figure 7.5.43 GC of the Oil/Dispersant Tank, 1 hr, fraction 5.

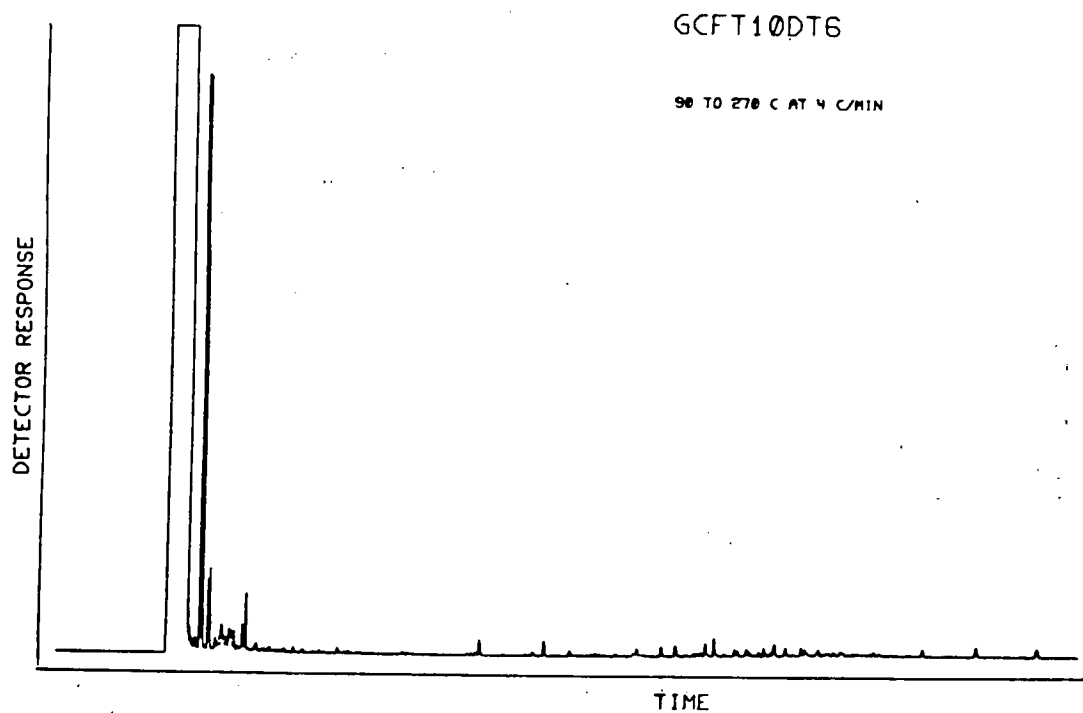


Figure 7.5.44 GC of the Oil/Dispersant Tank, 1 hr, fraction 6.

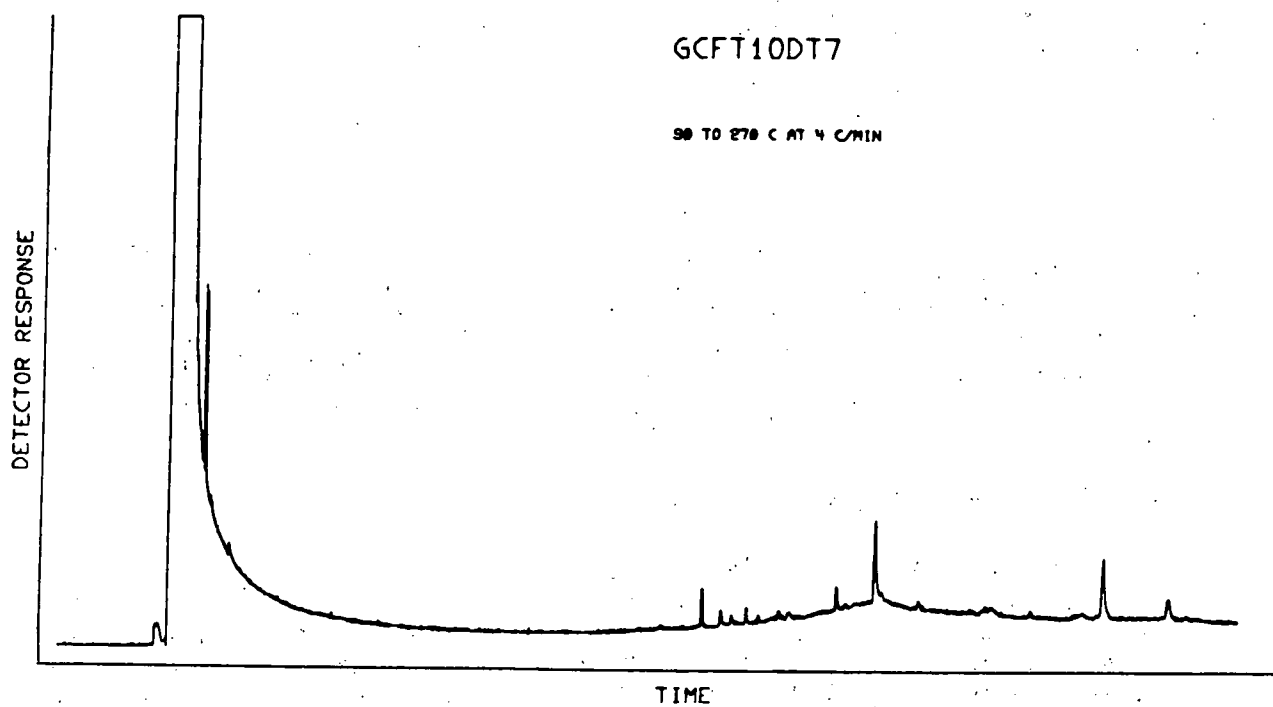


Figure 7.5.45 GC of the Oil/Dispersant Tank, 1 hr, fraction 7.

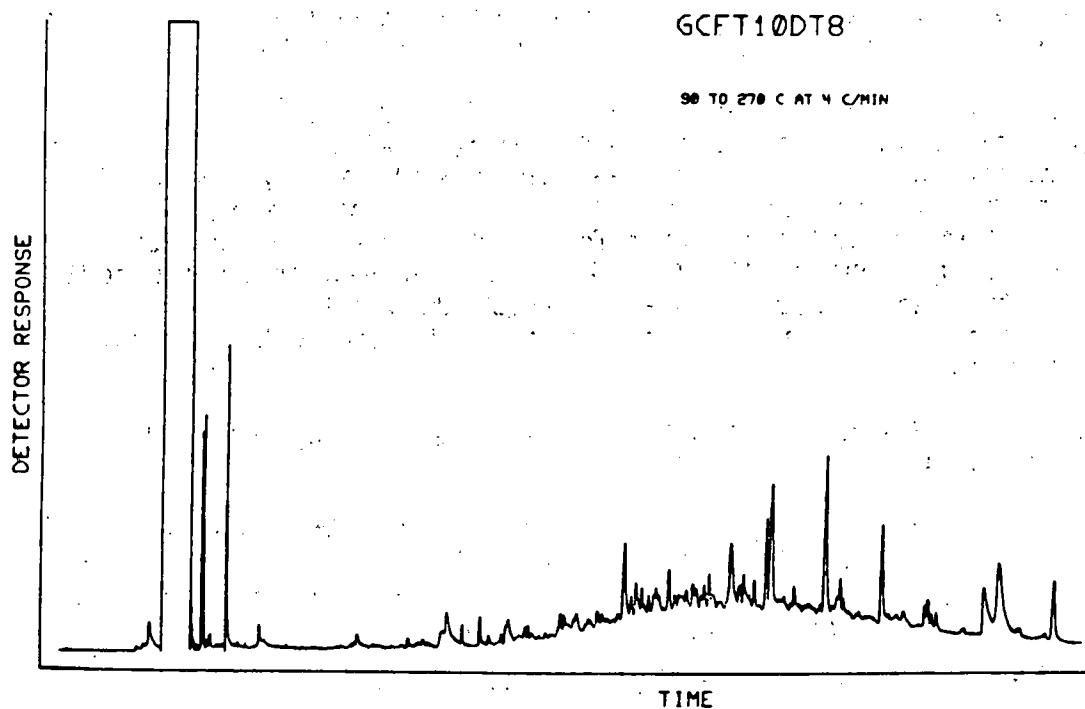


Figure 7.5.46 GC of the Oil/Dispersant Tank, 1 hr, fraction 8.

GC's of fractions 2 through 5 suggest increasing amounts of aromatics, whereas 6 through 8 go from the heavier aromatics to polars. It is interesting to compare the GC of the first fraction to that of the total material in Figure 7.5.10; a number of dissimilarities are observed. We also measured the GC of the surface slicks after five weeks of the experiment; these are shown in Figures 7.5.47 and 48. The GC of the first fraction is very similar to those of the surface slicks.

(C) Quantitative Analysis of Water Samples

Quantitative results for extractable organics in water samples are listed in Table 7.5.1. As mentioned previously, a 22% efficiency was used for the dispersant tank when the dispersant was present and a 65% efficiency when the dispersant was not detected. Very little dispersant was detected during week two; thus, the extraction efficiency is somewhere between 22 and 65%, and the values are lower than those in the table.

(D) Analysis of Sediment Samples

Sediment samples were collected from tanks 1, 3 and 4 on the first day and at the beginning of the fourth week. The quantitative results obtained by IR and GC are listed in Table 7.5.2. As in previous studies, the GC values are lower than the IR values; this is due to separation by thin layer chromatography between the IR and GC measurements. A very interesting fact is that the sediment values are lower in week four than in week one (except for tank 1 by GC). It should also be noted that the tank 4 (oil/dispersant) concentration was twice as high as the other two at the 1 hour sampling by the IR measurement. This is reasonable since most of the dispersant would be included in the IR measurement, but would be removed prior to the GC analysis by thin layer chromatography.

GC of the six sediment samples are shown in Figures 7.5.49-54. The pristane/phytane ratio in the control and the oil tank at one hour and in the GC of the control at the fourth week are greater than 1, whereas they are approximately one or less in the oil/dispersant at one hour and the fourth week and in the oil tank after four weeks. Thus, it appears that with the dispersant some of the petroleum hydrocarbons enter the sediments during the first hours. However, there does not appear to be a significant increase in petroleum hydrocarbons in the sediments during the three week period.

(E) Qualitative Analysis of Water and Slick Samples by Infrared Spectroscopy

Qualitative infrared spectra of all samples were measured from 1950 to 650 cm^{-1} . The IR spectra of the slick samples collected at the end of five weeks from the oil and dispersant tanks are identical, which is in agreement with the GC of the same two samples.

There are several noteworthy differences in the IR of the water samples. The infrared difference spectra of the sample from the top of the oil tank and from the top of the control tank at one hour is shown in Figure 7.5.55. Only one strong band appears at 1040 cm^{-1} . Although exact identification of the compound is not possible from one band, it

Table 7.5.1. Concentrations (ppb) of Extractable Organics in Water Samples from Flow-Thru Tank

		Experiments at Experimental Station in Jerusalem						
		<u>Week 1</u>	<u>Week 2</u>	<u>Week 3</u>	<u>Week 4</u>	<u>Week 6</u>	<u>Week 7</u>	<u>Week 9</u>
		<u>May 7</u>	<u>May 14</u>	<u>May 21</u>	<u>May 29</u>	<u>June 11</u>	<u>June 18</u>	<u>July 2</u>
1) Control,	Top	89	332	515	106	103	354	206
	Mid	326	342	416	76	116	369	
	Bot	89	356	507	75	110	246	
2) Oil,	Top	230	355	415	197	1170	436	166
	Mid	44	539	406	N.D.	1639	346	
	Bot	46	303	402	77	301	213	
3) Oil/Disp,	Top	3611	252	637	60	2066	318	201
	Mid	941	257	897	56	1834	330	
	Bot	304	2043	624	87	2235	333	
4) Disp,	Top	9598*	1215*	319*	99*	11,499*	352*	216*
	Mid	20082*	3071*	306*	104*	5,723*	306*	
	Bot	3992*	949*	515*	79*	1,344*	351*	

* 22% extraction efficiency used

+ 65% extraction efficiency used

N.D. non-detectable

Table 7.5.2
Concentrations ($\mu\text{g/g}$ dry weight) of Hydrocarbons
in Sediment Samples

Tank	IR Values		GC Values	
	Week 1	Week 4	Week 1	Week 4
	1. Control	36	17	6.8
2. Oil	29	15	6.9	4.4
3. Oil/dispersant	73	9	6.4	3.9

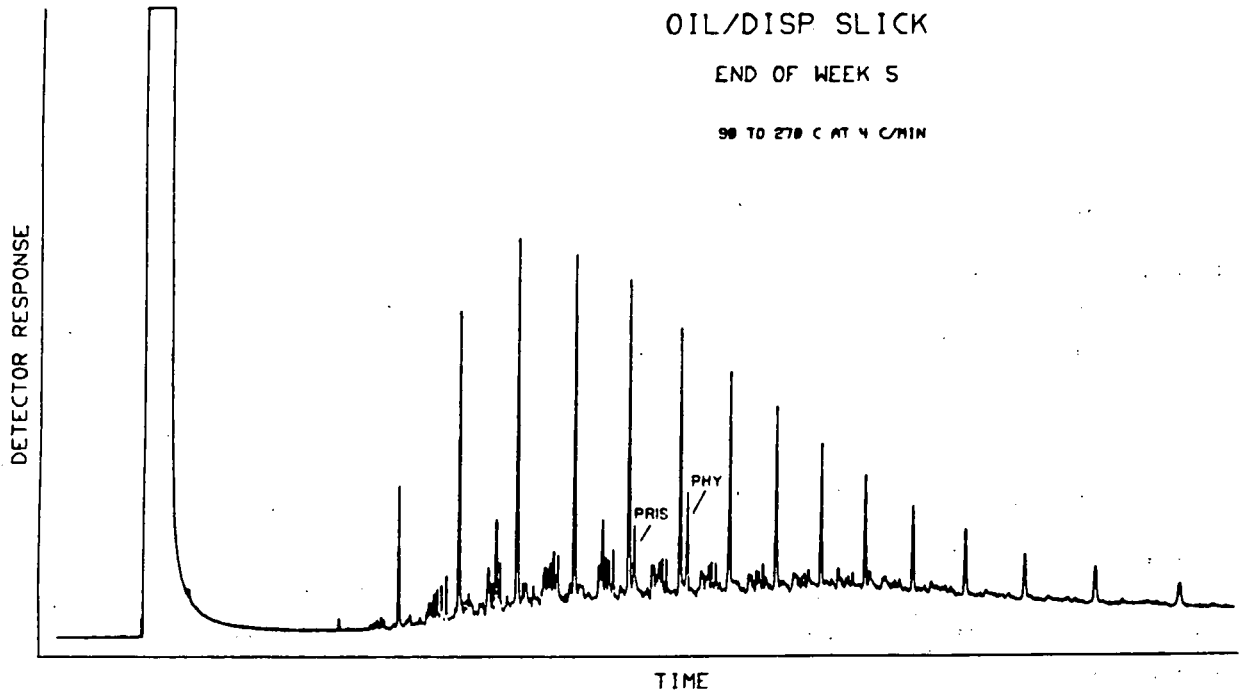


Figure 7.5.47 GC of the Slick in the Oil/Dispersant Tank, week 6.

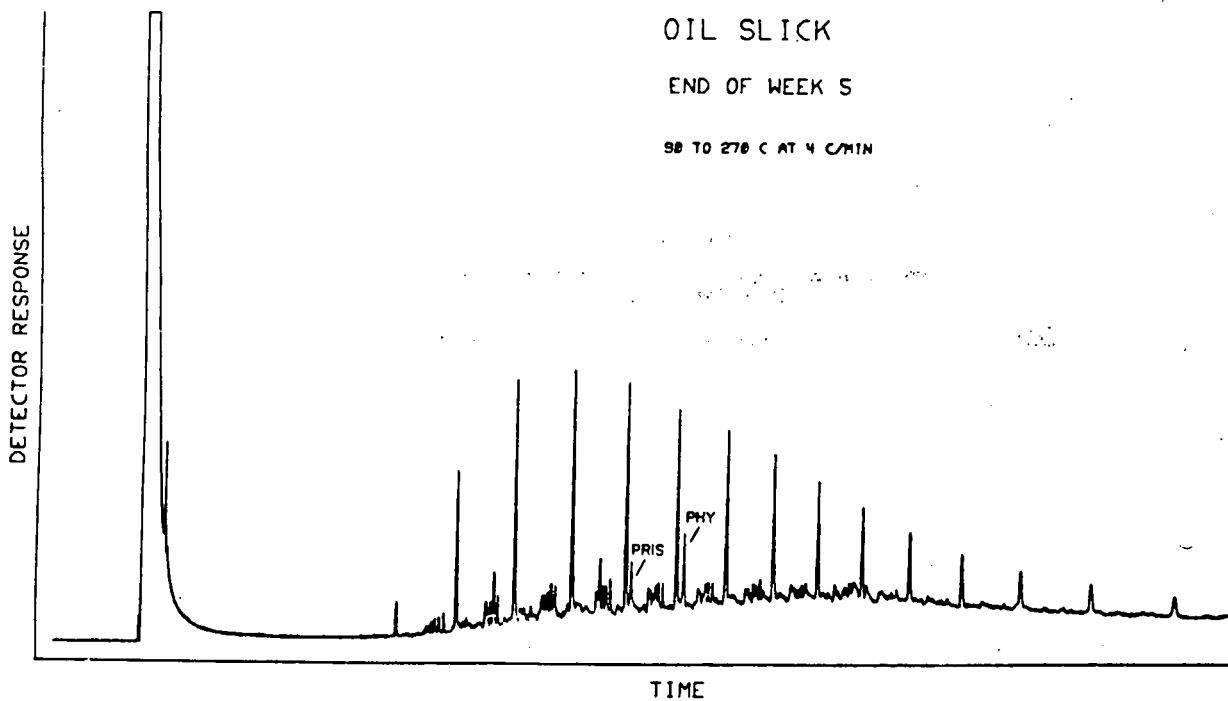


Figure 7.5.48 GC of the Slick in the Oil Tank, week 6.

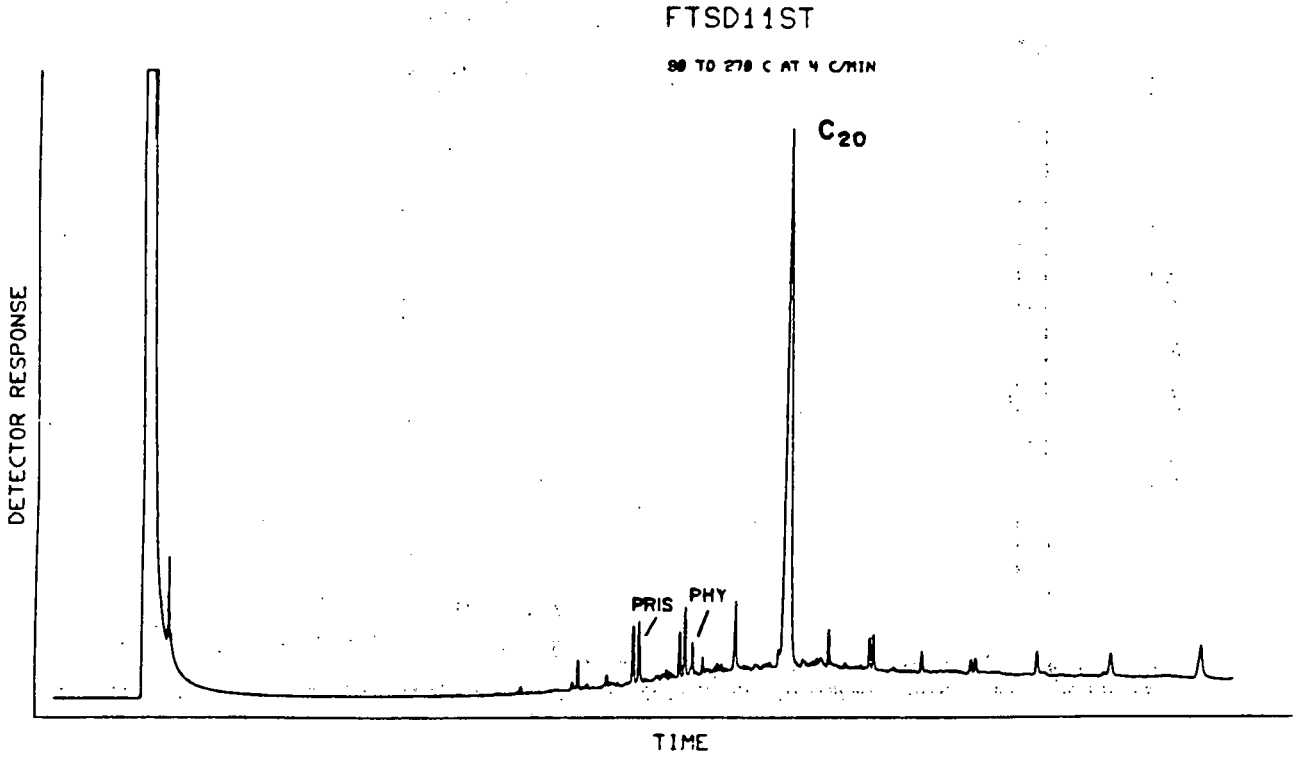


Figure 7.5.49 GC of the Sediment in Control Tank, 1 hr.

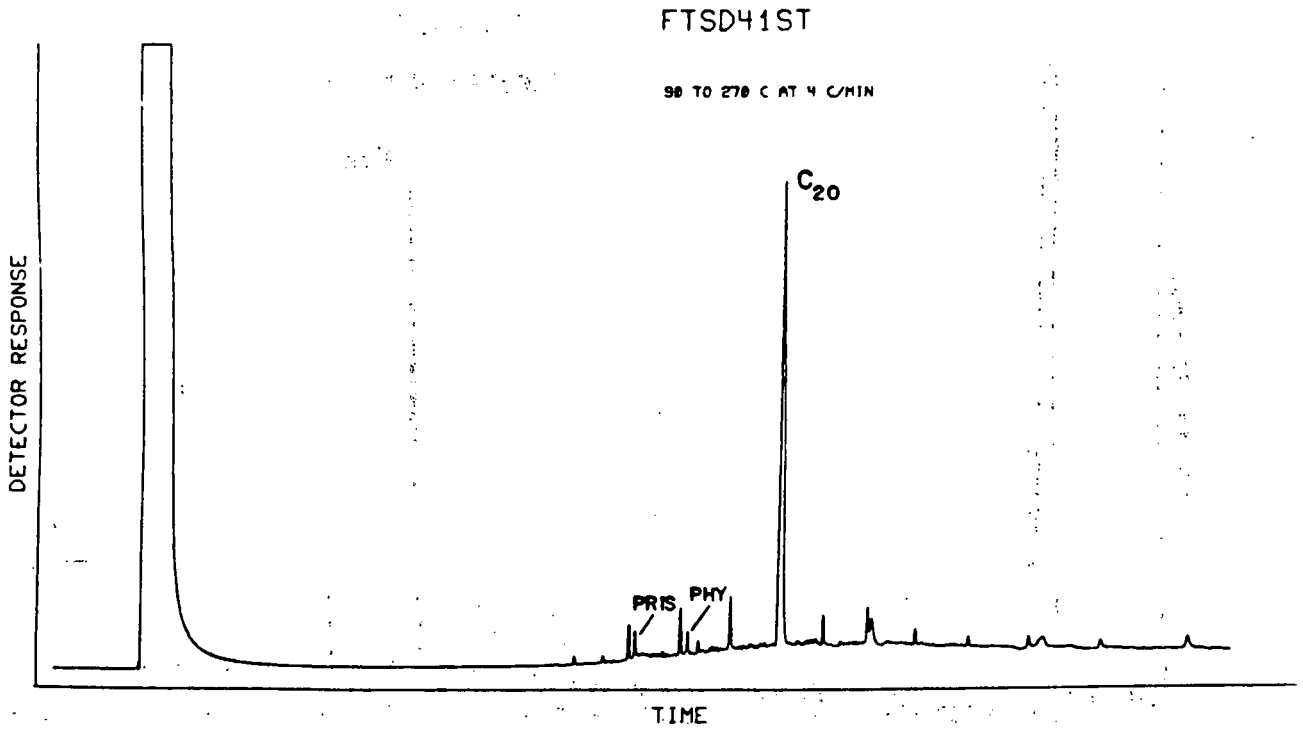


Figure 7.5.50 GC of the Sediment in Oil Tank, 1 hr.

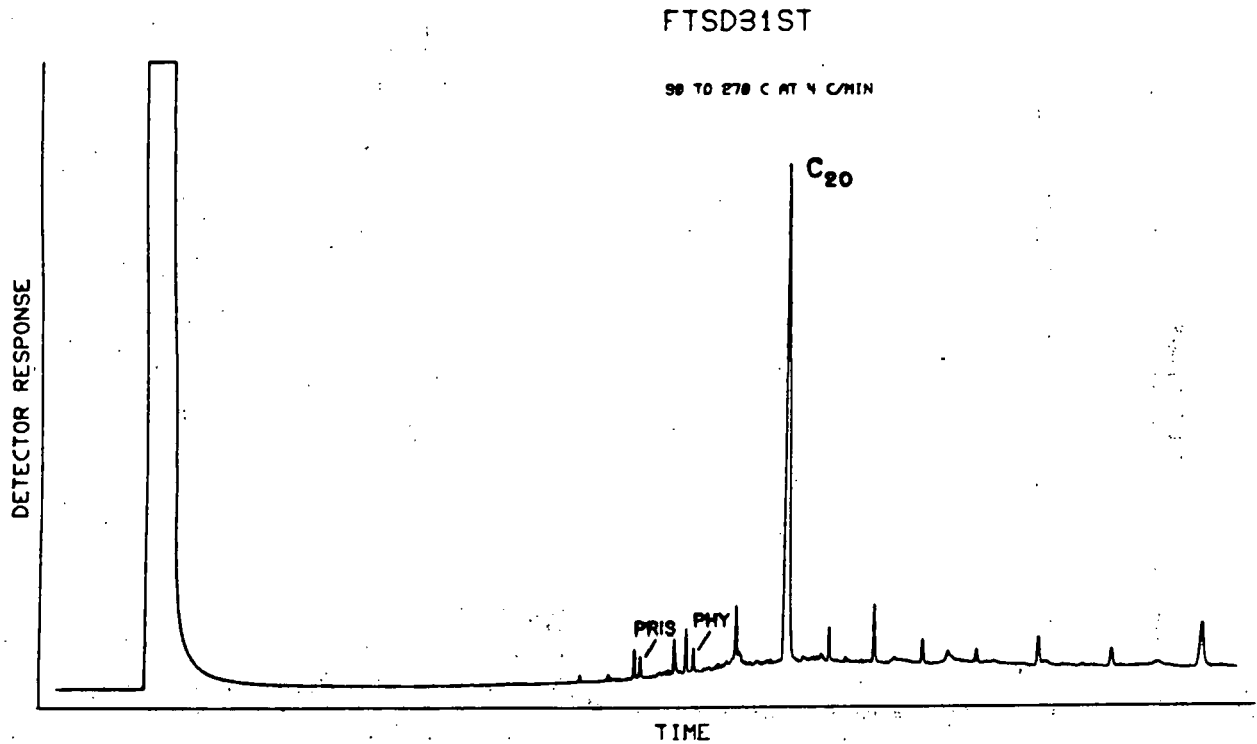


Figure 7.5.51 GC of the Sediment in Oil/Dispersant Tank, 1 hr.

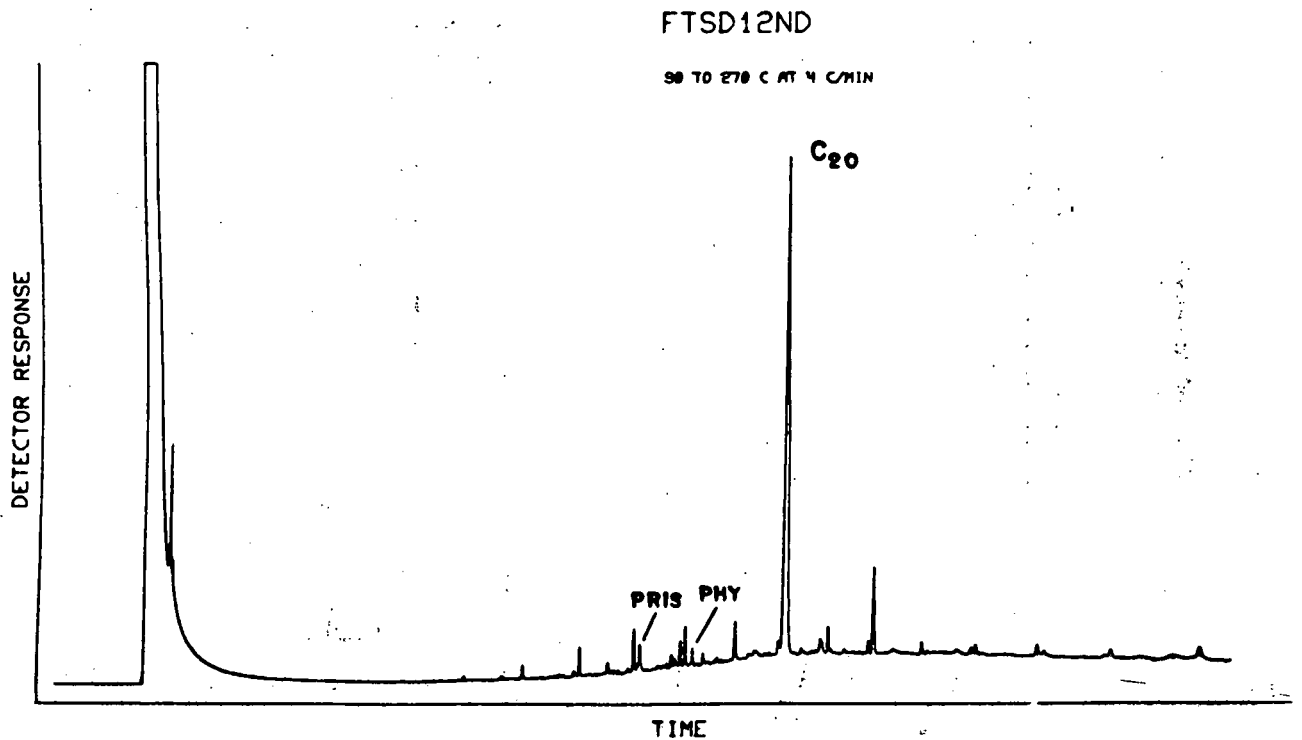


Figure 7.5.52 GC of the Sediment in Control Tank, 4th week.

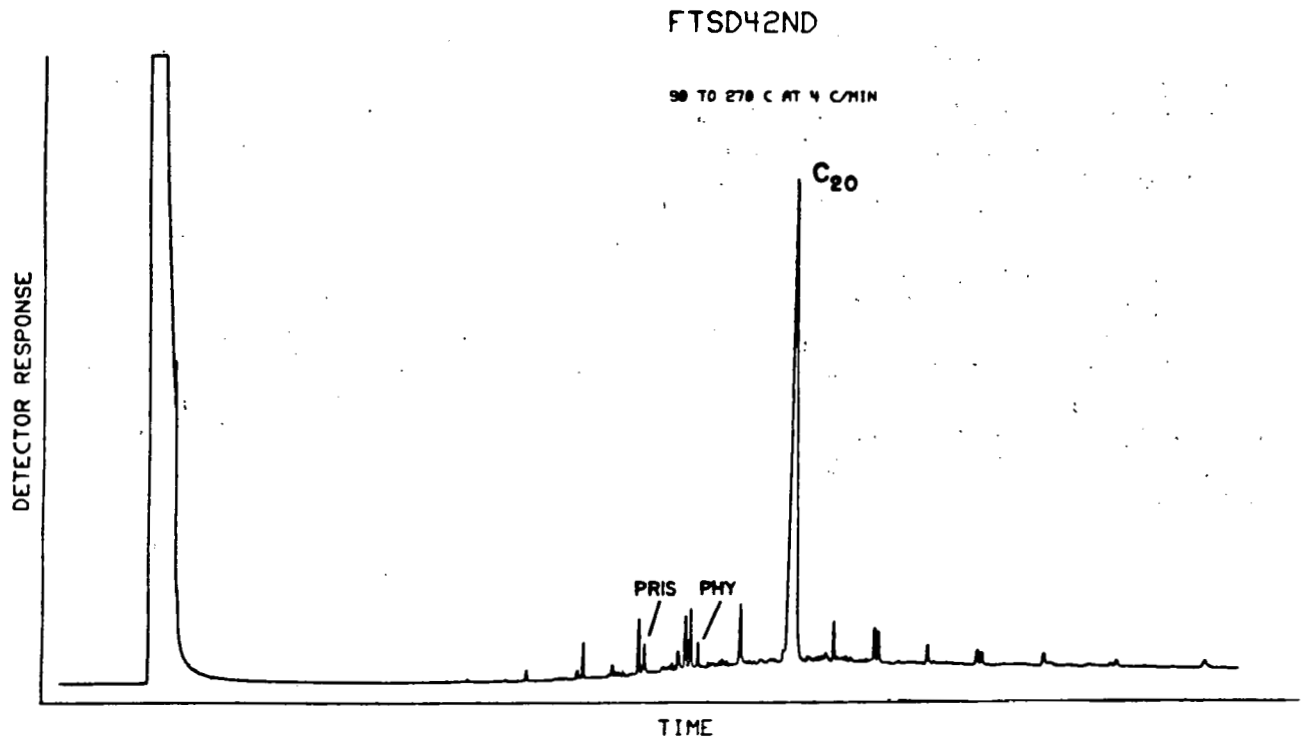


Figure 7.5.53 GC of the Sediment in Oil Tank, 4th week.

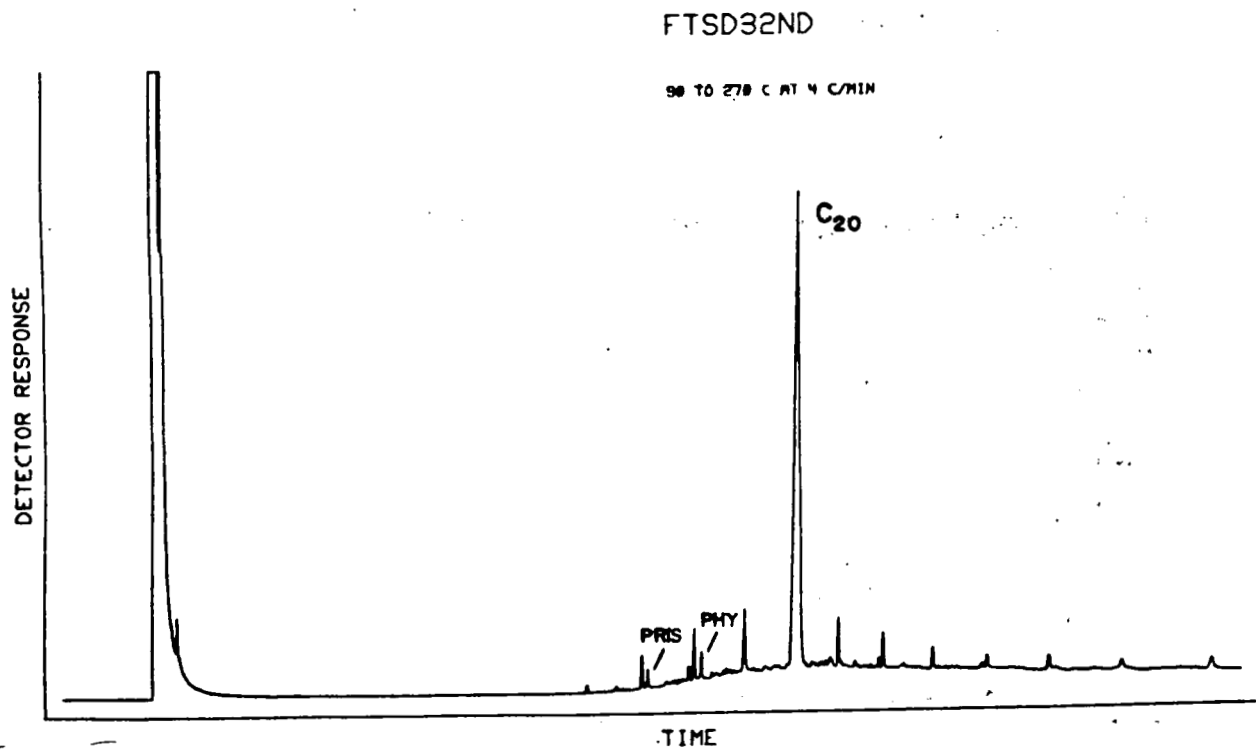
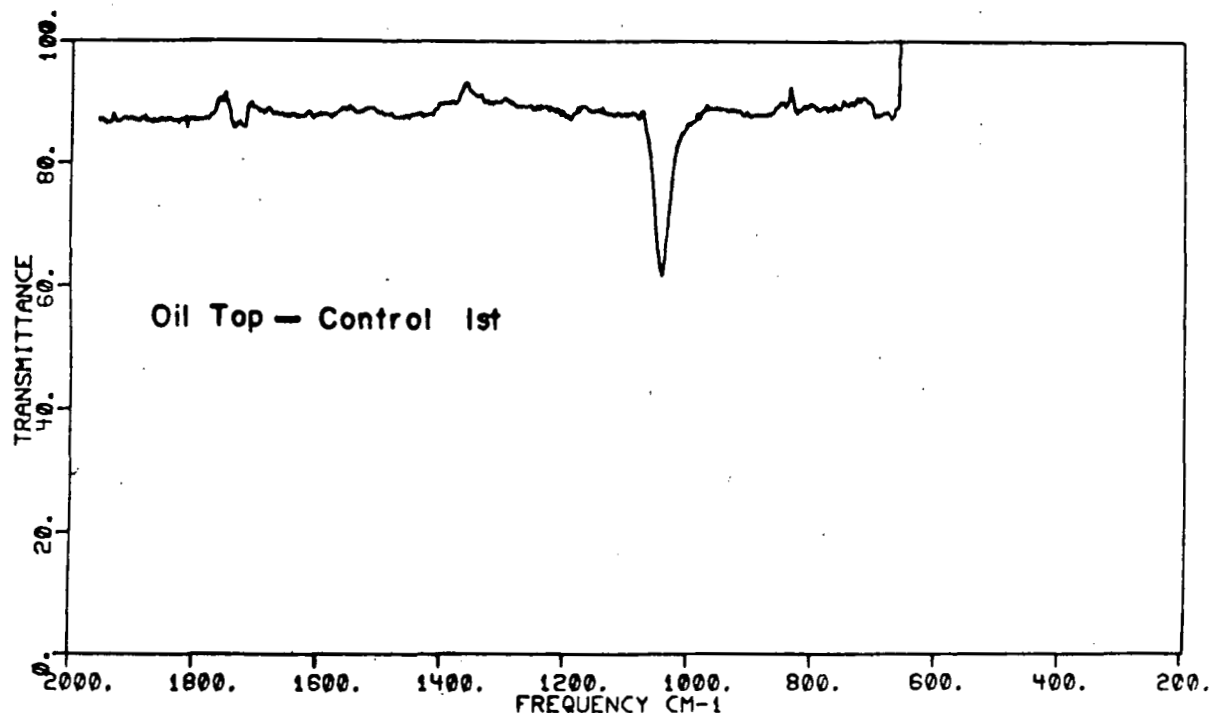


Figure 7.5.54 GC of the Sediment in Oil/Dispersant Tank, 4th week.

could well be a sulfoxide and the band due to the S=O group which absorbs strongly at this frequency. An organic sulfoxide could account for the tendency of this oil to form mousse and act as a self-dispersant. This band is also found in the difference spectrum obtained by subtracting the oil/dispersant middle from the oil/dispersant top at the first sampling as is shown in Figure 7.5.56.

Another interesting feature is found in the difference between the oil/dispersant and oil at the top after addition of dispersant in the sixth week as is shown in Figure 7.5.57. The peak at 770 appears only in the oil/dispersant spectrum; thus, it has a positive value (pointing down) in the difference spectrum. This peak was also observed in the top sample from the dispersant only tank. It may account for other differences observed between the tanks after the dispersant was applied a second time.

Figure 7.5.55 IR difference spectrum; top of oil tank minus top of control tank, 1 hr.



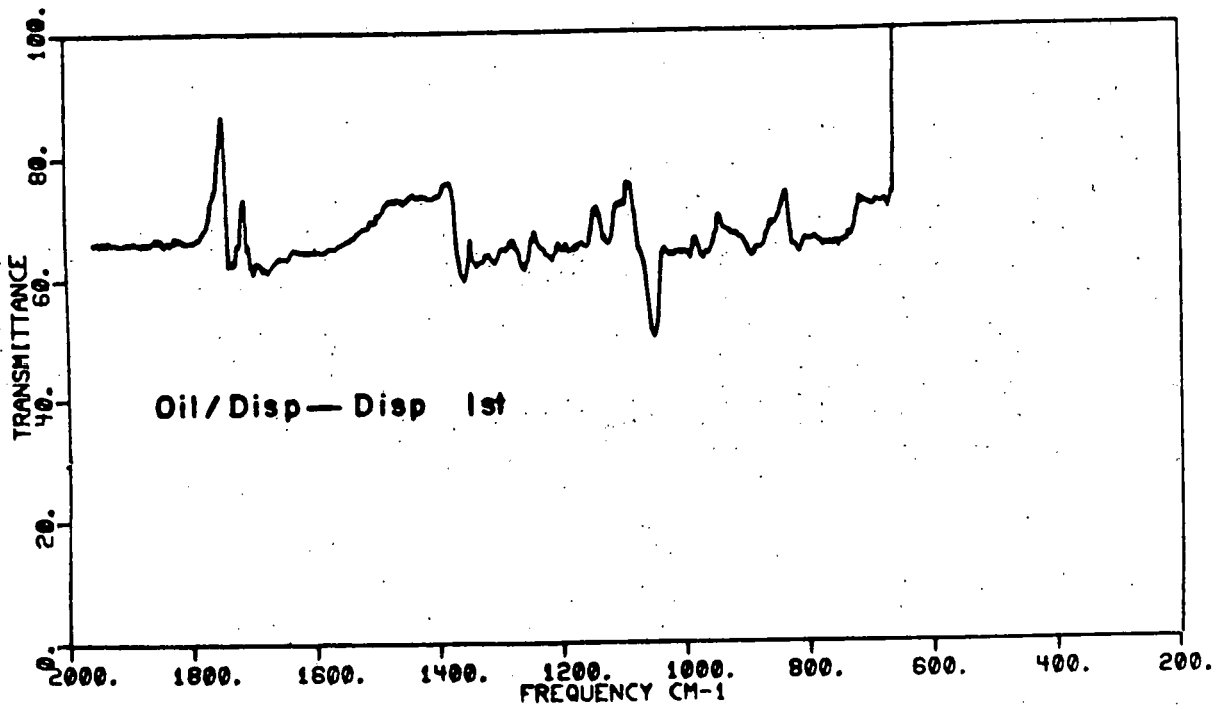


Figure 7.5.56 IR difference spectrum; oil/dispersant top minus oil/dispersant middle, 1 hr.

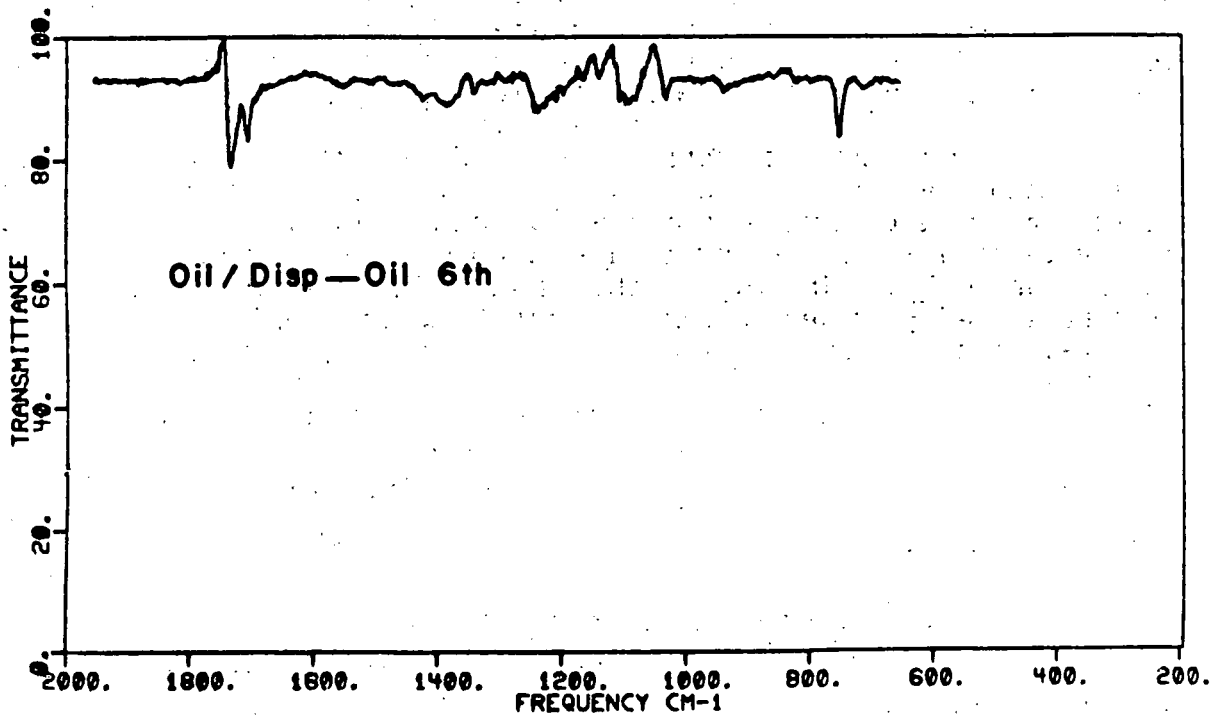


Figure 7.5.57 IR difference spectrum; oil/dispersant top minus oil top, 6th week.

7.6 Field Studies

7.6.1 Field Study of the Buzzard Bay Spill

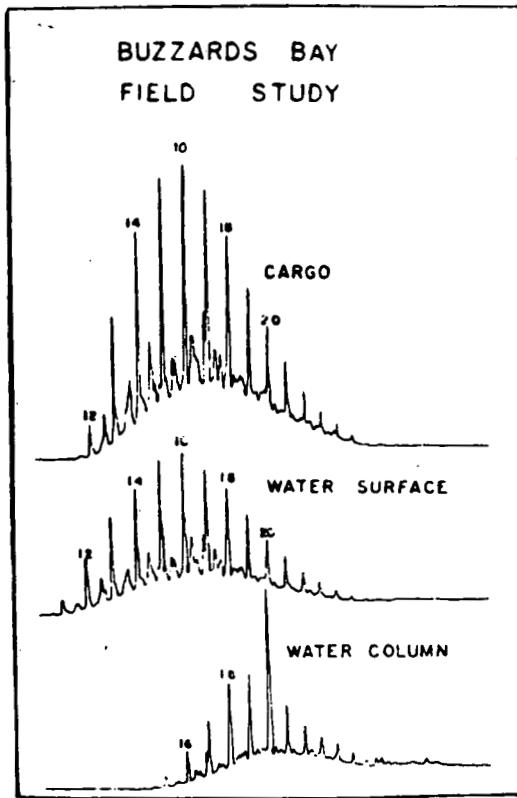
During the last week of January 1977, 100,000 gallons of a No. 2 fuel were spilled from a barge into the ice laden entrance to the Cape Cod Canal, i.e., in Buzzards Bay. The oil became trapped in and beneath the ice; thus this spill offered a unique opportunity to test our laboratory methodology on an actual spill. One week after the spill, we collected the following samples: oil in the ice, oil on the water, water samples at 3 m beneath the surface, and sediment samples with a grab sampler. Since the grab sampler had to be pulled through the surface water which possibly contained oil, we returned the following week and one member of the group collected sediment samples by diving beneath the ice. On this occasion an air sample was also collected on shore by pumping air through a charcoal cartridge for one hour.

All of the field samples were returned to the laboratory for analysis. We obtained a sample of the oil from the barge; the oil was analyzed and the results on the field samples were compared to those on the cargo oil and to the results of the laboratory experiments on the oil.

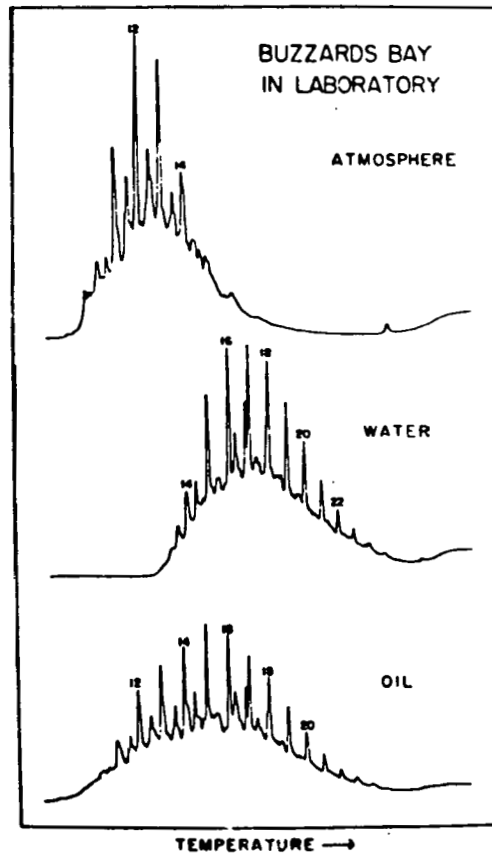
Oil was found in the water column and sediment samples. The infrared spectral fingerprints of the oil in the ice and on the water surface definitely matched the cargo oil. The spectral fingerprint of the oil in the water column was also very similar to that of the cargo; however, the fingerprint of the sediment hydrocarbons could not be directly related to that of the cargo. There are two possible explanations for this observation: the composition of the oil retained by the sediments could be considerably different from that of the cargo, or the hydrocarbons in the sediments could be from a different source. The latter explanation appears more reasonable, since the same barge spilled oil at this site in 1974. The amount of hydrocarbons in the sediments was relatively low. However, it should be mentioned that the sediment samples were very sandy and may not retain the oil as well as finer sediments.

Possibly the most interesting and useful results are on the air and water column samples. The gas chromatograms (GC) of the water column, water surface, and cargo samples are compared in Figure (7.6.1). The GC of the cargo and surface samples are virtually identical, e.g., note the doublet at $n\text{-C}_{17}$. The GC of the water column sample also has this doublet at $n\text{-C}_{17}$; however, only the higher boiling hydrocarbons can be observed in the GC of this sample. Fifty g of $n\text{-C}_{20}$ were added to this sample as an internal standard: thus, the $n\text{-C}_{20}$ peak is appropriately higher than those of the other $n\text{-paraffins}$. The latter GC should be compared to that of the laboratory water sample of the same oil which is shown in Figure 7.6.2. Both the field and the laboratory water samples show that only the hydrocarbons boiling at or higher than $n\text{-C}_{14}$ enter the water column.

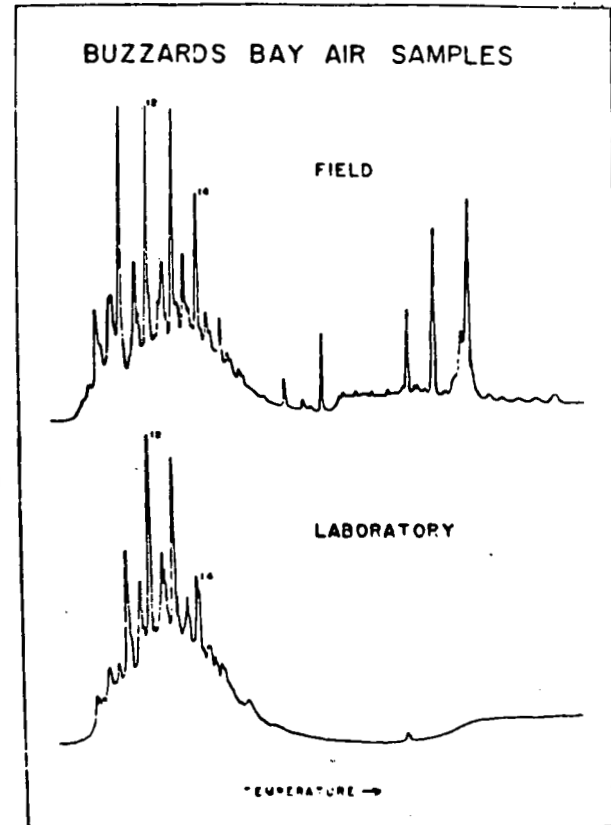
The air sample collected at Buzzards Bay offers even greater support to the laboratory results. The GC of the field and laboratory air samples are shown in Figure 7.6.3. Both show that the hydrocarbons entering the atmosphere are predominantly those boiling at or below $n\text{-C}_{14}$. There is a considerable similarity between the relative composition of



7.6.1 GC of the Buzzards Bay Oil, Cargo, Surface and Water Column.



7.6.2 GC from the Laboratory Experiment on the No. 2 Fuel Oil from the Buzzards Bay Spill



7.6.3 GC of Field and Laboratory Air Sample from the Buzzards Bay Oil.

the hydrocarbons in the two samples. The GC of the field sample does show some higher boiling chemicals. Possibly these are of biological origin and may be more polar than petroleum hydrocarbons which would account for their longer retention time on the GC column.

7.6.2 Field Study of the Argo Merchant Spill

Another spill of opportunity occurred during the early morning hours of December 15, 1976, when the Argo Merchant went aground in the Nantucket shoals. The tanker split and spilled its cargo of 7.7 million gallons of No. 6 oil into the sea. At about the same time, another tanker, the Grand Zenith, was lost at sea and was also carrying a No. 6 fuel.

Approximately 60 to 90 days after the grounding of the Argo Merchant, tarballs began to wash ashore on Jamestown (R.I.), Martha's Vineyard, Nantucket and Cape Cod (Mass.) (from Nauset Beach to Provincetown). This laboratory received and analyzed 22 of these tarballs ranging in weight from a few ounces to 15 lbs.

Table (7.6.1) lists the information on the tarballs which were analyzed. The samples, which contained aquatic debris and occluded water, needed to be pretreated and cleaned up prior to analysis. To do this, approximately 5 mls. of each sample were placed in a test tube and spun in a centrifuge for a few minutes, allowing the debris to separate to the bottom and the oil to rise to the top of the tube. The oil layer was then transferred to another test tube and 5 mls. of CCl_4 were added. The sample was then shaken well and centrifuged for five minutes. The top three-quarters of the sample was then transferred to another test tube, a drying agent, MgSO_4 , was added and the sample was again centrifuged for five minutes at 35°C . This last series of steps was repeated until all water was removed from the sample. The CCl_4 was then removed by evaporation.

The samples were then placed in a demountable infrared cell with a 0.05 mm spacer and the spectra were measured on a Perkin-Elmer 521 Infrared Spectrometer. The digitized spectral data were stored in a computer data file and all data analyses were performed on an IBM 370/60 computer.

Kileen and Chien (1) proposed a method for obtaining the probability of matching spilled oil to one or more suspects from infrared spectra of the samples. Their method is an extension of the ratio method developed in our laboratory (Ahmadjian et al., 2).

In the ratio method, absorbances at 18 frequencies in the spectrum of one sample are ratioed with absorbances at the same frequencies in the spectrum of another sample. The log of each ratio, the average log-ratio, and the differences between each log-ratio and the average log-ratio are determined. Initially, we ratioed the absorbances in the spectrum of each suspect to those in the spectrum of the spill sample; the best match was assigned to the spectrum having the most ratios within 10% of the average. Later, the method was extended to give a single value for estimating the differences between spectra (2). This value is obtained from the sum of the squares of the differences between the

Information on Tar Balls

Tar Ball No.	Site	Date	Comment
1	Jamestown, R.I.	2/9/77	a, ~1 lb., composite
2	Jamestown, R.I.	2/9/77	a, ~1 lb., outside
3	Jamestown, R.I.	2/9/77	a, ~1 lb., inside
4	Jamestown, R.I.	2/9/77	b, ~5 lb., inside
5	Jamestown, R.I.	2/9/77	c, ~15 lb., inside
6	Martha's Vineyard	2/12/77	
7	Nantucket	2/15/77	
		to	
8	Nantucket	3/1/77	
9	Nantucket	3/1/77	
10	Nantucket	3/1/77	
11	Nauset Beach	3/1/77	
12	Nauset Beach		No. 11 weath. at GSO
13	Marconi Beach	3/1/77	
14	Marconi/Lecount	3/14/77	
15	Race Pt. Beach	2/10/77	Sewage
16	Race Pt. Light	3/1/77	
17	1000 yds. from Race Pt. Light	3/1/77	
18	Long Pt.	3/12/77	
19	Provincetown Wharf (a)	3/15/77	
20	Provincetown Wharf (b)	3/15/77	
21	Pilgrim Beach (a)	3/12/77	
22	Pilgrim Beach (b)	3/12/77	

Table 7.6.1
Information on Tar Balls

log-ratios and the average log-ratio, i.e.,

$$S^2 = \frac{18}{\sum_{i=1}^{18}} \left(\log \frac{A_{i1}}{A_{i2}} - \frac{1}{18} \sum_{i=1}^{18} \log \frac{A_{i1}}{A_{i2}} \right)^2$$

where A_{i1} and A_{i2} are the absorbances for the i th band in spectra 1 and 2, respectively. For a perfect match, the value of S^2 would be zero; thus, the magnitude of S^2 reflects the dissimilarity between oils.

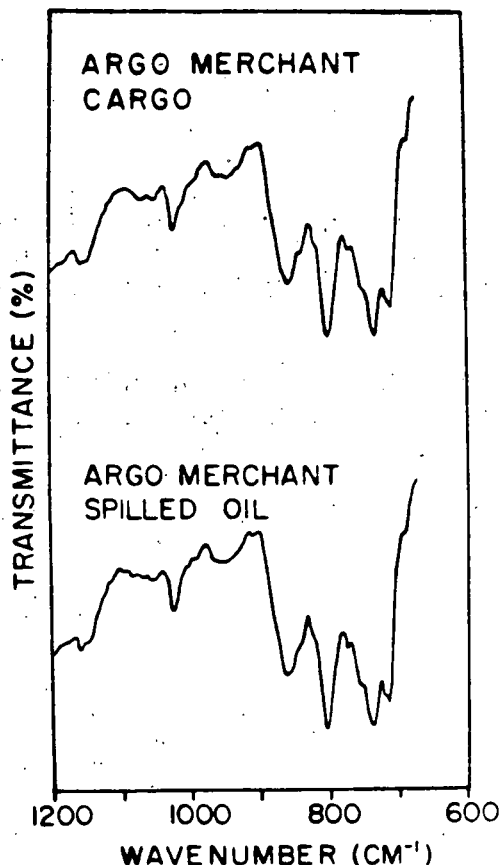
We (2) measured spectra of 198 neat and 647 weathered oils (including several weathered samples for each of 80 neat oils). S^2 values for all possible pairs of oils were calculated and placed in one of two categories: same oils (neat and weathered oils from the same origin) and different oils (neat and weathered oils from different origins). There were 5,534 pairs with the two oils originating from the same source, and 345,030 pairs with the two oils from different sources. The pairs in each category were then ordered according to increasing S^2 values, and two histograms for frequency of occurrence vs. S^2 in increments of 0.01 were plotted.

The histograms provided distributions for pairs of oils from the same sources and for pairs from different sources. Kileen and Chien (1) used these distributions to determine the probabilities of guilt for each suspect in a spill case and the probability that a sample from the "true spiller" was not included. Their method is based on Bayes Theorem and is described completely in their report (1).

In the present report, it is important to note that the distributions used to obtain the probabilities are based on all types of oils, i.e., they are comprised of light through heavy crudes, fuels and lubricating oils. This tends to give slightly higher probabilities especially at the low end of the 0 to 1 probability scale. For example, infrared fingerprints of two No. 6 fuels may be completely different and we would expect that the probability that they match would be close to 0.0; however, since they are both No. 6 fuels, their fingerprints will be more similar than the fingerprints of a No. 6 and No. 2 fuel. Thus, in many cases, the probability that two different No. 6 oils match will be higher than expected because they are the same type of oil.

Infrared spectra of the Argo Merchant cargo and of the spilled oil collected two days after the tanker broke apart are shown in Figure (7.6.4). (These samples were obtained from Dr. Jerome Milgram, MIT). When the digitized spectrum of the spilled oil was compared with that of the cargo, the following probabilities were obtained:

	<u>Probability</u>
Argo Merchant	0.986
Another Source	0.014



Infrared Spectra of the Argo Merchant Cargo and of the Spilled Oil Collected 2 Days After the Spill.

Infrared spectra of the 22 tar balls listed in Table (7.6.1) were measured and the digitized fingerprints stored in a computer data file. Many of the spectra had similar contours and some were almost identical as is shown in Figure (7.6.5). The spectrum of each tar ball was compared with that of each of the others and the probability that they came from the same source is given in Table (7.6.2). The results are categorized according to magnitude in Figure (7.6.6).

All samples from Jamestown, Martha's Vineyard and Nantucket have probabilities >0.85 of being identical except for sample 2 from Jamestown. This was a sample of the outside layer of a tar ball, and the differences reflect excessive weathering on the surface. In addition to samples 1-10 being from the same source, the probabilities that samples 12, 16, 17 and 19 came from this source are >0.5 . Furthermore, tar balls 11 and 13 are virtually identical ($P=0.99$).

It should be mentioned that the differences between many of the tar balls could be due to weathering and that this effect is more pronounced on the surface of the tar balls. Many of the tar balls from Cape Cod were very small and these could have been subjected to extensive weathering.

The infrared spectral fingerprint of the Argo Merchant oil is compared to that of the Martha's Vineyard tar ball in Figure 7.6.7. The general contours of the spectra are entirely different. We treated each of the 22 tar balls as a spill sample and determined the probability that each came from the cargo. The results given in Table 7.6.3 show that only sample No. 11 (Nauset Beach) had a probability of matching >0.3 ; most were <0.2 . The spectrum of the cargo and the tar balls (except for sample 15) were characteristic of No. 6 fuel oils. Thus, these finite probabilities reflect the fact that the samples are the same type of oil.

If the tar balls came from the Argo Merchant, they were "weathered" in the Atlantic for almost two months; thus, we weathered some of the cargo oil at the URI aquarium for one month and periodically analyzed the samples. In most cases, the spectra of the tar balls and weathered Argo Merchant tar balls became less similar. The probability of matching for the 3 and 10 day samples are also given in Table 7.6.3.

The tanker, Grand Zenith, disappeared somewhere off the New England coast on the way from Teeside, England to Fall River, Massachusetts during January 1977; thus, its cargo was also a possible source of the tar balls. The U.S. Coast Guard R & D Center supplied us with a sample of the oil loaded aboard the Grant Zenith. We measured infrared spectra of the neat oil and of samples collected periodically during one month of weathering at the URI aquarium. The infrared spectrum of the Grand Zenith oil is compared with the Argo Merchant cargo and the Martha's Vineyard tar ball in Figure 7.6.8.

The probabilities obtained when comparing the spectra of the neat and 7 weathered samples to the tar balls are given in Tables 7.6.4a and b. The probabilities run as high as 0.83 when the neat oil is compared to tar balls No. 3 and 4; however, the highest probability (90) was obtained from matching the 14 day weathered sample with tar ball No. 11 from Nauset Beach (see Figure 7.6.9 for spectra). Other tar balls found in

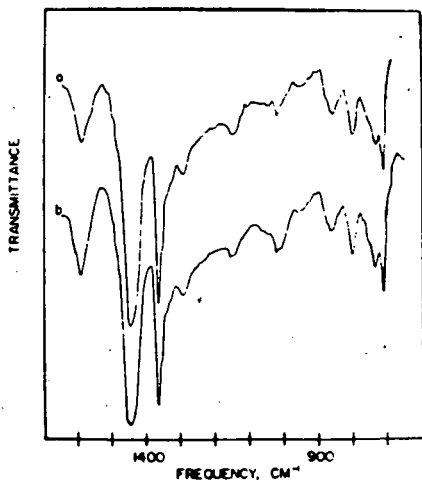


Figure 7.6.5 Infrared Spectra of Tar Balls:
a. Jamestown and b. Martha's
Vineyard.

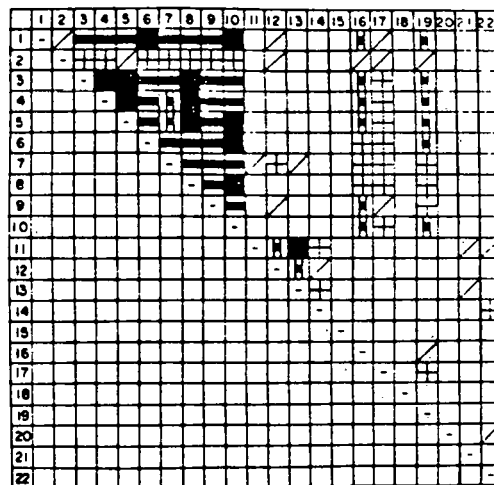


Figure 7.6.6 Probabilities of Tar Balls Matching.

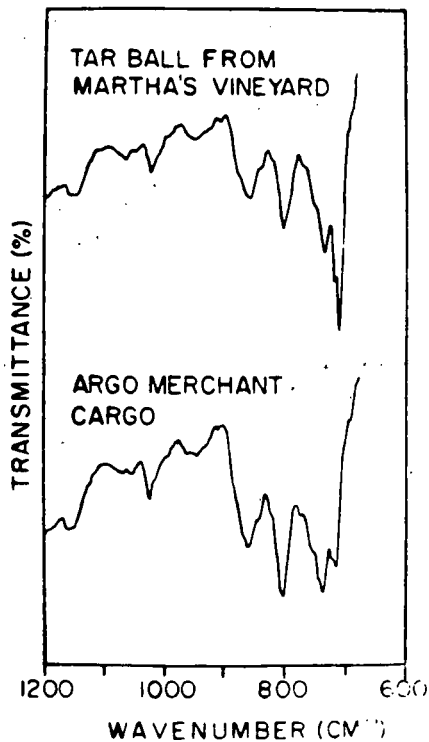


Figure 7.6.7 Infrared Spectra of Tar Balls
from Martha's Vineyard and Argo
Merchant Cargo.

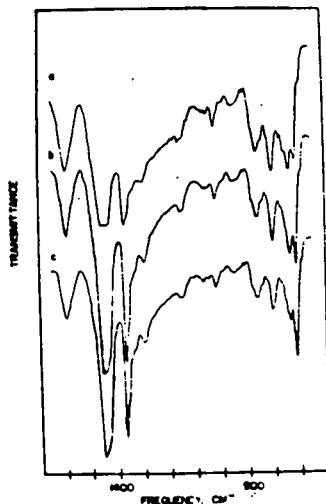


Figure 7.6.8 Infrared Spectra: a. Argo Merchant Cargo, b. Grand Zenith Oil and c. Martha's Vineyard Tar ball.

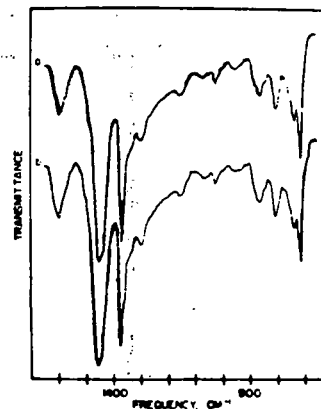


Figure 7.6.9 Infrared Spectra: a. Tar ball from Neuset Beach and b. Grand Zenith Oil weathered 14 days.

Probabilities of Tar Balls Matching (in % Units)

	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22
1	-	66	96	96	97	99	95	97	97	99	46	55	43	20	0	86	66	16	89	16	27	18
2		-	76	70	67	79	77	77	71	71	45	56	41	33	0	56	51	16	59	18	19	20
3			-	96	100	97	96	99	97	98	38	45	36	18	0	90	77	20	91	17	19	18
4				-	100	98	93	100	97	99	33	41	31	18	0	87	83	17	90	16	18	17
5					-	97	93	99	98	100	35	42	34	15	0	90	80	20	91	14	18	18
6						-	98	98	97	99	47	60	44	22	0	84	76	17	89	18	22	18
7							-	95	98	95	55	72	53	26	0	74	73	16	82	18	28	19
8								-	96	99	38	48	35	19	0	84	84	19	84	16	17	18
9									-	97	45	50	42	21	0	91	63	16	73	17	23	18
10										-	40	48	38	19	0	91	76	18	86	16	20	18
11											-	94	99	81	0	33	23	21	33	34	55	53
12												-	94	57	0	31	37	18	44	32	39	36
13													-	80	0	31	23	19	33	32	54	48
14														-	0	18	18	21	18	44	36	71
15															-	0	0	0	0	0	0	0
16																-	25	16	58	15	20	19
17																	-	0	70	16	17	17
18																		-	22	19	19	43
19																			-	15	18	17
20																				-	25	55
21																					-	44
22																						-

TABLE 7.6.2 Probabilities of Tar Balls Matching

Probability of Tar Balls Originating From Argo Merchant Cargo
(In % Units)

Tar Ball	Near	Argo Merchant Cargo	
		3 Days Weathered	10 Days Weathered
1	22	18	18
2	18	25	18
3	21	5	18
4	19	0	18
5	20	0	18
6	20	7	18
7	19	19	18
8	20	22	18
9	21	23	18
10	21	20	18
11	32	18	32
12	23	18	27
13	27	19	27
14	18	18	18
15	0	0	0
16	21	0	18
17	15	17	16
18	18	16	18
19	18	25	18
20	18	25	21
21	19	18	22
22	22	18	28

Table 7.6.3 Probability of Tar Balls Originating From Argo Merchant Cargo

Table A
Probability of Tar Balls Originating From Grand Zenith Cargo
(In % Units)

Tar Ball	Grand Zenith Cargo Weathered (Days)			
	0	1	2	4
1	74	77	75	51
2	45	45	52	55
3	83	87	86	66
4	83	87	88	69
5	82	85	86	63
6	73	75	76	57
7	60	65	70	52
8	76	81	81	58
9	89	73	73	44
10	79	83	83	55
11	36	35	38	31
12	38	38	42	41
13	32	33	35	30
14	18	18	18	18
15	0	0	0	0
16	75	78	77	40
17	33	37	40	44
18	14	16	16	20
19	71	75	74	81
20	16	16	16	15
21	18	18	20	19
22	18	18	18	18

Table B
Probability of Tar Balls Originating From Grand Zenith Cargo
(In % Units)

Tar Balls	Grand Zenith Cargo Weathered (Days)			
	7	14	21	28
1	73	55	26	27
2	58	47	33	34
3	77	50	22	24
4	75	49	20	21
5	76	47	20	21
6	77	58	29	29
7	70	63	35	34
8	72	47	23	23
9	74	61	29	30
10	78	54	25	26
11	55	90	86	87
12	51	73	64	58
13	47	84	81	83
14	23	41	87	77
15	0	0	0	0
16	85	58	23	26
17	32	24	18	18
18	17	19	18	21
19	59	37	18	20
20	18	22	37	30
21	27	46	61	63
22	22	40	58	64

Table 7.6.4 A. Probability of Tar Balls Originating from Grand Zenith Cargo Weathered 0-4 days
B. Probability of Tar Balls Originating from Grand Zenith Cargo Weathered 7-28 days

this area (Nos. 13 and 14) have probabilities of 0.85 of matching the weathered Grand Zenith oil.

According to the probabilities given in Table 7.6.4, the tar balls can generally be placed into three categories: i) those with high probabilities of matching the neat or short term weathered samples, ii) those with high probabilities of matching the long term weathered samples, and iii) those with low probability matches. Samples 1,3-10, 16 and 19 fall in category i, samples 11-14, 21 and 22 in category ii, and the rest in iii.

The study showed conclusively that the tar balls found along the New England coast after the Argo Merchant incident were not from the stricken tanker. Many of the tar balls had similar infrared spectra and there is a high probability that a number of these came from the same source. Finally, there is a reasonably high probability that some of the tar balls originated from the stricken tanker, Grand Zenith. It should be noted that the tar balls were compared with oil loaded onto the Grand Zenith, and not to the oil actually contained in the tanker. The composition of the oil in the tanker could have been slightly different due to residues in the tanker from previous shipments.

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Titles and Authors

Computer Separation of Infrared Spectra for Analysis of Complex Organic Mixtures, P.F. Lynch* and M.M. Brady.

Predicting The Performance of Medium and Low Resolution Infrared Spectrometers and Analyzers, Chris W. Brown, Patricia F. Lynch and Mark A. Maris and Donald S. Lavery.

Quantitative Analysis of Gaseous Hydrocarbons By Infrared Spectroscopy, Chris W. Brown, Patricia F. Lynch and Mark A. Maris and Donald S. Lavery.

Computerized Infrared Spectroscopy as a Separation Technique-Analysis of Complex Organic Mixtures Extracted from Water, P.F. Lynch, and M.M. Brady.

Collection, Separation and Analysis of Organic Vapors by Computerized GC/IR, D. Goldfarb and C.W. Brown.

Chemical Analysis of Dispersed Oil in the Water Column, C.W. Brown,¹ P.F. Lynch,¹ and M. Ahmadjian.¹

Collection of Gas Chromatographic Fractions on Activated Charcoal and Identification by Infrared Spectroscopy, Daniella Goldfarb and Chris W. Brown.

Computerized dispersive infrared spectroscopy gives results comparable to FTIR, as we perform "Festa of Magic," Dr. Chris W. Brown, Patricia F. Lynch and Mark Ahmadjian.

In the Wake of the Argo Merchant, Center for Ocean Management Studies.

8.0 Microbiology

Richard W. Traxler

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8.0 MICROBIOLOGY

8.1 Introduction:

The report of a special study group of the National Academy of Sciences on Petroleum in the Marine environment (1) indicated that the rates of microbial degradation of petroleum hydrocarbons vary with the complexity of the material, the nature of the microbial population and environmental conditions. The physical process of dispersion of a spilled oil will reduce the concentration of oil in the spill vicinity and greatly increases the surface area of the oil which renders the oil more susceptible to biological degradation (2).

The hydrocarbon degradation potential of ocean environments has not been adequately defined (3) but is known to be influenced by such factors as the number and types of hydrocarbon degrading microorganisms, the degree of oil dispersion, temperature and nutrient availability (4). Hydrocarbon degradation rates measured in the laboratory have been misleading as they were found to be considerably higher than in situ rates (5). It has been demonstrated (6) that degradation rates in cold waters are reduced compared to warmer water but not to the extent previously thought. Surfactants have been investigated as a mechanism to increase oil recovery (6),(7) and microorganisms have been shown to actively emulsify hydrocarbons (8), (9) and oils (10). Studies have shown that chemical dispersants stimulate bacterial growth on oil and the biodegradation of the oil (11).

This project was designed to investigate the effect of chemical dispersants on the ability of natural marine bacterial populations to biodegrade crude oil hydrocarbon components.

8.2 Materials and Methods:

8.2.1 Culture Media

The culture media used in the project were:

1. Nutrient Seawater Agar (NSA)

NaCl	21g.
Rila Salts	5g.
Polypeptone	5g.
Yeast Extract	3g.
Glucose	1g.
Succine Acid	.2g.
K ₂ HPO ₄	.33g.
KH ₂ PO ₄	.66g.
Agar-Agar	16g.
Distilled Water	1 L.

2. OZR Agar

Yeast Extract	1g.
Trypticase	1g.
Fe PO ₄ 2H ₂ O	10mg.
Agar-Agar	16g.

Aged Seawater *pH 7.8 1 L.

3. Hydrocarbon Basal Medium (HBM)

Aged Seawater	990ml.
Supplement B*	10ml.
Washed Agar-Agar**	20g.
*Supplement B	
NH ₄ Cl	7.5g.
FE PO ₄ 2H ₂ O	4.75g.
Distilled Water	250ml.

*Narragansett Bay water (GSO site), cheesecloth filtered to remove particular matter and aged one month in the dark in glass carboys.

**Flaked agar was soaked and rinsed three times a day with tap water for three days, and once a day for the next five days, followed by once a day rinses in distilled water for six days, then air dried and ground to powder.

The sterile melted agar was placed in a sterile Waring Blender, the hydrocarbon added at desired concentration, blended at high speed for three minutes and poured into sterile plates.

8.2.2 Dissolved Oxygen, Azide modification for BOD.

1. Solutions

- a. Manganese Sulfate
MnSO₄ H₂O, 91g. in 250 ml distilled water, filter and dilute to volume.
- b. Alkaline-iodide-azide reagent

NaOH or KOH	250g.
NaI or KI	67.5g.
NaN ₃	5g.

Dissolve NaOH and NaI in distilled water, dilute to 500ml, then add NaN₃ dissolved in 20 ml distilled water.

- c. Sulfuric acid 36N
- d. Starch
- e. Sodium thiosulfate

NaS₂O₃ 5H₂O (0.1N), 24.82g. dissolved, boiled, cooled, then distilled water added to 1000ml, add 5ml of chloroform as a preservative.

2. Method

Remove 200 ml of water from the BOD bottle, add 2ml of $MnSO_4$ and 2 ml of alkaline-iodide-azide reagent. Shake and let stand for at least two minutes, add 2 ml of H_2SO_4 and shake until the ppt is dissolved. Titrate with sodium thiosulfate until pale straw color, add 2 ml of starch solution and titrate until the purple color disappears.

3. Modified BOD Method

For the standard BOD method a standard inoculum is prepared for addition to each bottle and the measurement of O_2 used provides an estimate of organic matter in the water. The modification was to use the natural seawater microbial population as inoculum and challenge this population with a known quantity of substrate. A control was used for each series which consisted of the seawater without added nutrient. This provides an estimate of oxygen depletion caused by the natural microbial population metabolizing the endogenous nutrients present in the seawater. This value was subtracted from the test results. All samples were run in triplicate and the average value used as the data point.

The results are reported as rates of oxygen depletion for a given microbial population at any time during the course of the experiment. A series of at least 21 BOD bottles containing the same water and challenge substrate are set up for each water sample. Three bottles are selected at random for any measurement time during the rate determination and measured for dissolved oxygen content.

8.2.3 Radioactive Degradation Rate Determination

Substrates labeled with ^{14}C carbon are used as an auxiliary method to determine the rate at which materials are degraded by natural microbial populations. Several different approaches have been used to estimate turn-over of hydrocarbon components. The metabolic $^{14}CO_2$ produced from the metabolism of the ^{14}C substrate was trapped at hourly intervals to calculate rate of CO_2 production. Another approach was to measure rate of CO_2 release, and rate of production of water soluble intermediates and end products. ^{14}C -Hexadecane was used as a representation n-alkane, ^{14}C -Naphthalene as representative of low molecular weight aromatic compounds and ^{14}C -Benzopyrene as a representative of high molecular weight aromatic compounds. The ^{14}C -hydrocarbons were used either at constant value (luci) or added to samples in the approximate ratio in which they occurred in the oil under investigation.

The reaction vessels were 250 ml flasks fitted with a CO_2 free air sweep to carry metabolic CO_2 into the methanol-ethanolamine traps, or the same type of flask fitted with a rubber cap. In the latter case, the reaction vessel was incubated for three hours, acidified with 0.1N HCL to release all bicarbonate as CO_2 which was then flushed from the reaction vessels into CO_2 traps.

The flasks were extracted with n-pentane at acid pH to recover all residual hydrocarbon and any lipids produced during the reaction. The pentane extracted seawater was counted to measure low molecular weight, water soluble products left after the extraction. The pentane extract was then partitioned with acidified methanol: ethanol (1:1) to remove lipids from the pentane extract. The pentane and alcohol were counted

for ^{14}C activity.

The specific radioactivity of the substrate is known, therefore, it is possible to convert the radioactivity in the various products by calculation to ng. of substrate utilized. If the initial amount of hydrocarbon is known, the turnover time of the substrate can be calculated using equation 1.

Equation 1.

$$T/F = \frac{\text{Time/ng Hydrocarbon metabolized}}{\text{ng Hydrocarbon added}}$$

The degradation time of a complex mixture such as crude oil can be estimated using equation 2.

Equation 2.

$$D/F = \frac{\text{Time/ng component a + ng b + ---}}{\text{Total Petroleum present}}$$

8.2.4 Viable Plate Counts

The plates for "total heterotrophic" bacterial counts (THB) and Hydrocarbonoclastic Bacteria counts (HYB) were prepared and incubated at least 24 hours but not over 96 hours at the temperature at which the experiment would be performed. This allowed proper drying of the agar surface to reduce spreading of the bacterial colonies as they developed on the agar surface. All glassware and diluents were held six hours at experiment temperature to prevent temperature shock to the bacteria.

Plating was performed via the spread plate technique which consisted of spreading 0.1 ml of the proper dilution over the entire agar surface using a sterile glass rod bent into the shape of a hockey stick. Samples were serially diluted and three consecutive dilutions of each sample were chosen for spread plating. The normal dilutions used were 10^{-1} , 10^{-2} and 10^{-3} but higher dilution values were used in some cases to achieve countable plates (30-300 colonies). In most experiments, two dilutions were prepared from each sample and two plates were spread from each dilution which means we had four plates for counting at each data point. This method increases the statistical accuracy of the spread plate count method. The values reported are the numerical average of the four plates.

The plates were counted on a Quebec Colony Counter with transmitted light. Plates with opaque media were counted on the same instrument but using an oblique light source.

8.2.5 Most Probable Number Technique

This method was performed with OZR and HBM medium without agar. Five parallel series of dilutions were made for each sample, utilizing four decimal dilution series. One ml of each dilution was added aseptically to 10 ml of medium. Five control tubes of medium were used as a contamination check. All work was performed in a hood system to prevent air

contamination of the medium.

The tubes were incubated at the temperature chosen for the experiment and scored as growth or no growth. Growth was positive if there was visible bacteria on the tube bottom, throughout the medium, or underlying the hydrocarbon (oil) phase.

The number of positive tubes in each dilution of the five parallel series was determined and the number of bacteria per ml of sample determined using the MPN tables of Postgate (1969).

8.2.6 Replica Plating Technique

This technique was described by Pierce, Cundell, and Traxler (1975). The bacterial colonies from the master plate (obtained during viable plate count experiments) were transferred to other substrate plates using a velvet replicator pad (Fig. 8.1). The replication sequence was master plate to non-substrate basal agar, to hydrocarbon substrate to OZR agar. Colonies growing on the non-substrate basal agar were not scored when growing on a hydrocarbon substrate as they were considered to be growing at the expense for agar-agar rather than the hydrocarbon. The final OZR plate was used to insure that inoculum was carried forward from each colony.

8.2.7 Laboratory Experiment System

This system consisted of 5.5 gallon aquaria containing a 5 cm sediment base and fresh seawater overlay. A large glass tube extended into the midpoint of the water samples so that a pipet could be inserted to remove water without contact with the surface oil. Sediment samples were obtained with a tube within a tube arrangement. A large glass tube was placed in the water prior to the addition of oil and/or dispersant. When ready to sample the sediment, this tube was pushed into the sediment zone and a second smaller sterile tube was passed through the first glass tube to remove the sediment sample.

8.3 Results and Discussion

Three general purpose media were compared for use in the enumeration of "total" marine heterotrophic bacteria and as a base for a selective medium for hydrocarbon utilizing bacteria. The comparison of the three media to support growth of marine heterotrophic bacteria is shown in (Figure 8.2). OZR medium was superior to the other two media and was chosen as the basic medium for this study. Media K and G are both formulated using Rila Salts mix to replace the aged seawater of the OZR medium. It is apparent from these data that Rila Salts do not adequately substitute for aged seawater and that media so formulated provide much poorer productivity of the heterotrophic marine bacteria.

A comparison was made of the viable plate count (VPC) and most probable number (MPN) methods for enumerating marine heterotrophic bacteria in OZR medium. Both methods (Figure 8.3) were capable of determining increases in the number of bacteria. The MPN method did yield slightly higher total numbers, but still within the range of statistical variation. It was found that much greater logistical demands occurred with the MPN method to achieve the same accuracy as the VPC method. Also, it

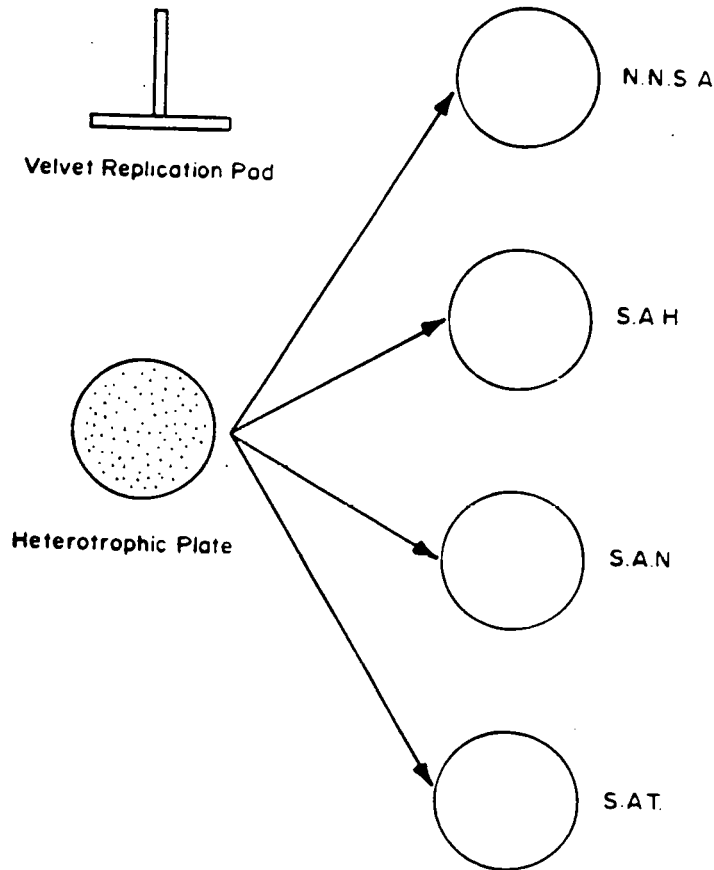


Fig. 8.1 Replicate Plating Technique

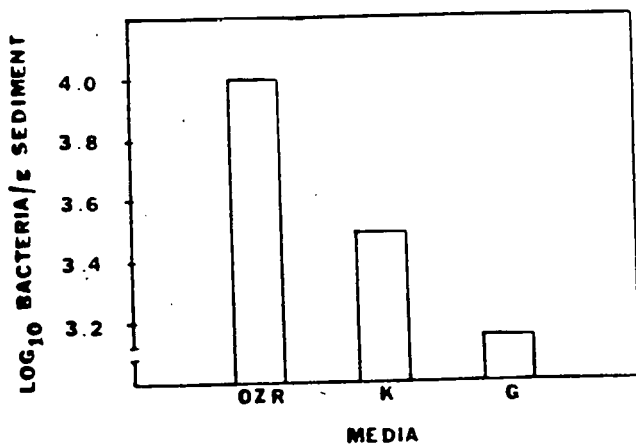


Fig. 8.2 Comparisons of Three Media for Ability to Support Growth of Marine Heterotrophic Bacteria

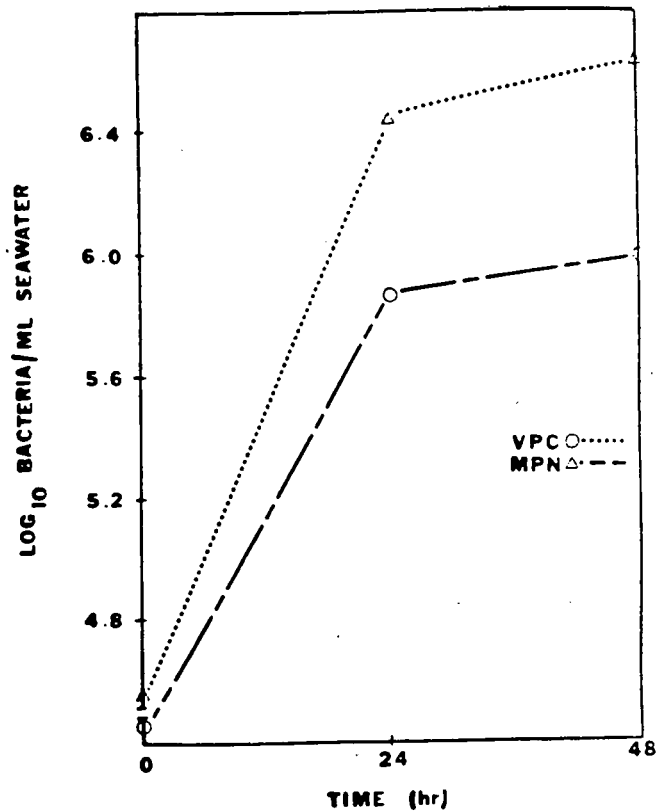


Fig. 8.3 Comparison of Most Probable Number (MPN) and Viable Plate Count (VPC) Methods for Enumerating Marine Heterotrophic Bacteria.

was desirable to have colonies on solid media for other aspects of the project. Therefore, the VPC method using OZR medium was chosen as the standard heterotrophic bacteria enumeration method.

The VPC was used with OZR and HBM media to estimate the relative percentage of hydrocarbon utilizing bacteria in the total heterotrophic population. This method was applied to seawater supplemented with Kuwait Crude oil dispersed with Corexit 9527. The relative percentage of oil degraders with the "total" heterotrophic population increased with time (Figure 8.4).

Biodegradation of a specific organic compound is most accurately measured by determining the rate of disappearance of the compound. When the study involves degradation of multiple substrates or a chemically complex material such as crude oil, the analytical chemistry required for the component loss approach is extremely complex and is drastically reduced in accuracy. The project objectives dictated a rapid, simple system which would provide a reasonable estimate of biodegradation potential. In an aerobic environment, all degradation reactions are associated with oxygen utilization, therefore we utilized a modified Biological Oxygen Demand (BOD) procedure which provided the rate and extent of oxygen depletion by the mixed sea water population on various substrates

Five tanks were filled with fresh untreated seawater at 14°C. Four tanks were loaded with one percent (weight/volume) of either n-hexadecane, naphthalene, Willimar crude or peptone. The fifth tank served as a control. The tanks were mechanically agitated to disperse the chemicals throughout the water column, then the water distributed into BOD bottles, which were incubated at 14°C. Oxygen levels were determined from duplicate bottles over the time course of the experiment.

The results are presented in Figure 8.5. The control value represents microbial utilization of the indigenous nutrients present in the seawater. These nutrients were exhausted after two days with a total oxygen depletion of 2 mg. The rates of oxygen depletion with the substrates were linear for an initial time period, then decreased in rate for a second time period. The depletion rates are summarized in Table 8.1. Peptone (used to express "total" biodegradation potential) showed the greatest depletion rate and completely utilized all available oxygen by day six. The oxygen depletion rates with Willimar crude oil and naphthalene were the same and it is noticed that the rates were higher than for hexadecane. The breakpoints in the oxygen depletion plots all occur at about 2 mg O₂ per liter and are believed to represent the point of oxygen limitation for the mixed population. In this experiment, mechanically dispersed substrate was introduced into the BOD bottle at extremely high substrate concentrations (10,000 mg/liter) which cannot be compared to in situ conditions but did serve to validate the modified BOD method.

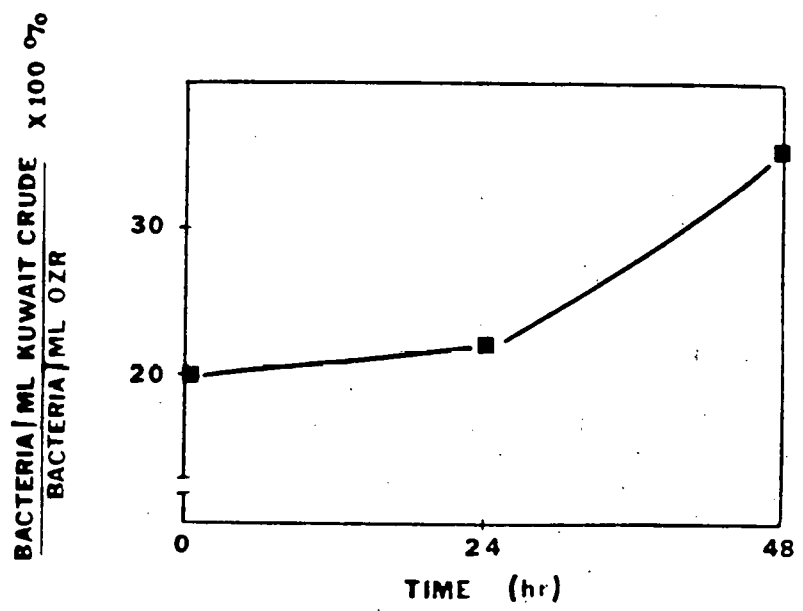


Fig. 8.4 Percentage of Marine Heterotrophic Bacteria Capable of Metabolizing Kuwait Crude Oil Agar Compared with OZR Medium.

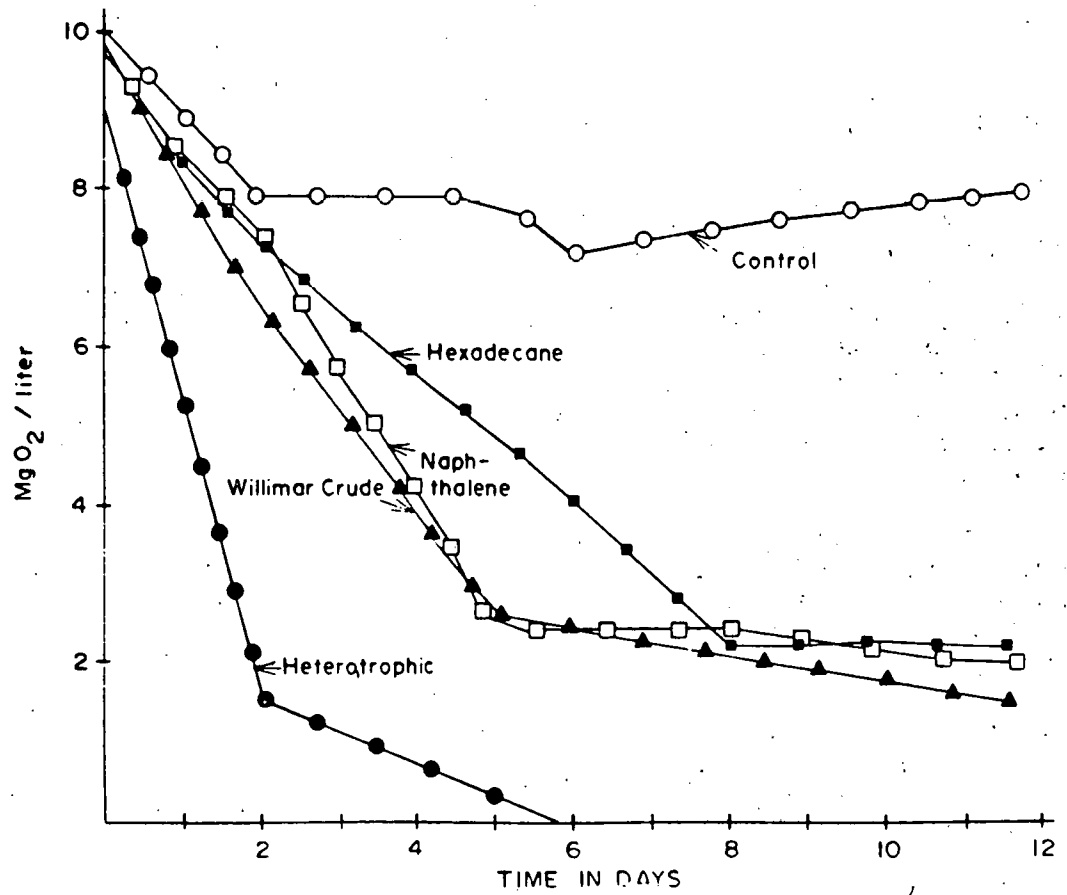


Fig. 8.5 Oxygen Depletion Rates of Various Substrates using a Modified BOD Method.

TABLE 8.1 RATE OF SUBSTRATE DEGRADATION, BY OXYGEN DEPLETION

Substrate	O ₂ mg/liter/day
Control (natural)	1.0
Peptone	3.5
Willimar Crude	1.25
Hexadecane	.94
Naphthalene	1.25

The experimental procedure was modified by eliminating mechanical mixing energy except for a gentle agitation of the tanks to simulate wave action. The tanks were filled with seawater and overlaid with API reference South Louisiana crude oil, the dispersant Corexit 9527, and a 10:1 mixture of crude oil and dispersant. Samples were removed from the center of the tanks after 24 hours for BOD measurements. Figure 8.6 shows the oxygen depletion for 24 hour samples from each of the four tanks. There was no oxygen utilization in the control tank, which indicated that the indigenous nutrient had been depleted during the 24 hour incubation prior to sampling the tanks. There was no depletion of oxygen in the South Louisiana crude tank, indicating either an absence of substrate in the water column or the inability of the resident bacterial population to utilize solubilized hydrocarbons. The absence of substrate was indicated from the results in the oil-dispersant tank.

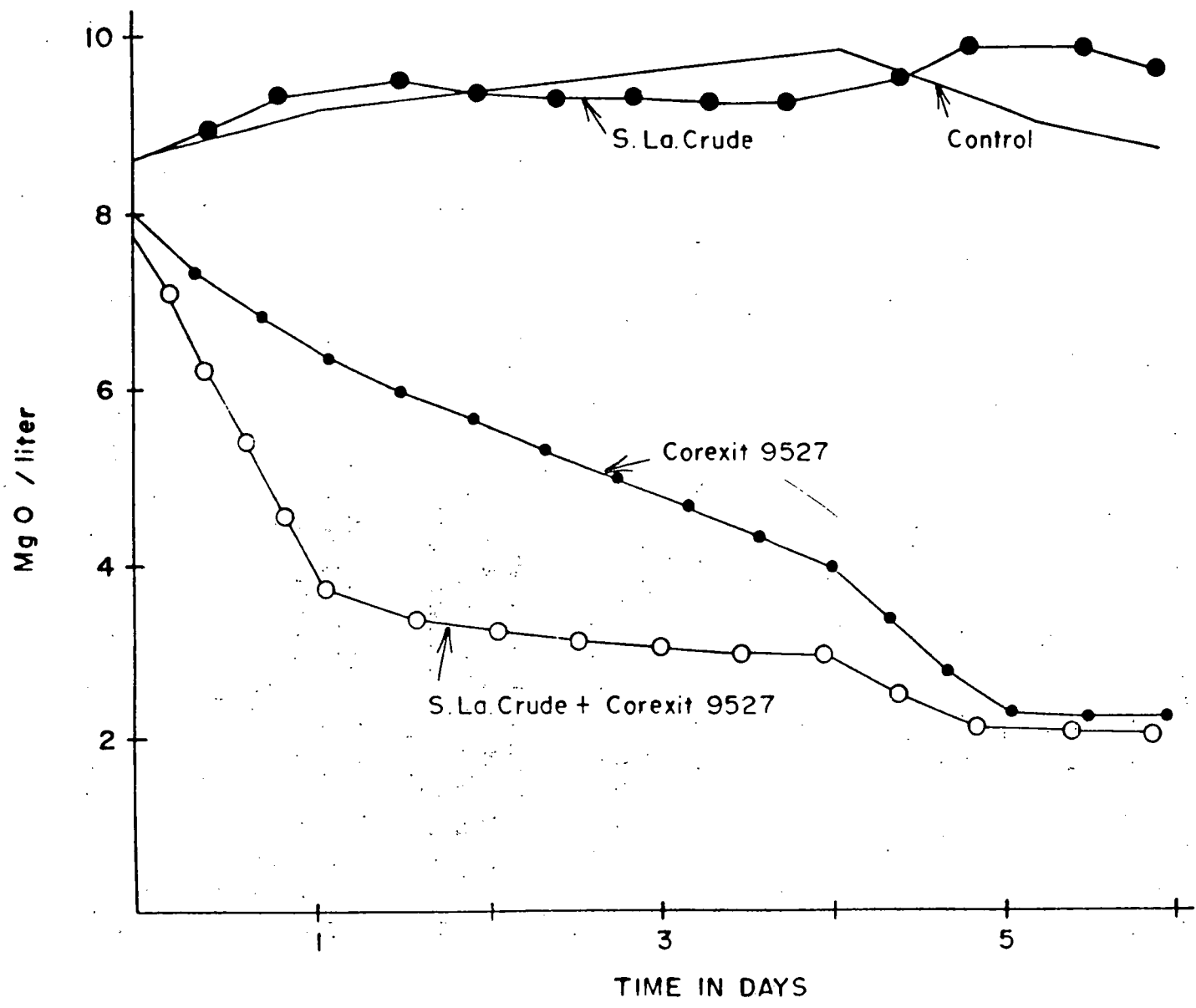
The biodegradable nature of Corexit 9527 was indicated by the oxygen depletion study, in which the oxygen was depleted at a rate of 1 mg O₂/liter/day. The oxygen depletion rate was much greater (4.25 mg/liter/day) with the mixture of crude oil and dispersant. This effect is apparent when considering no water column activity with just the crude oil and the much lower rate for the dispersant alone. The dispersant action would carry oil into the water column in small droplet form, in which it would be more readily available to the bacterial population.

It is interesting to note in these experiments as well as replications and other studies with the oxygen depletion method that the final oxygen level is always about 2 mg of O₂/liter. This would infer that microbial action on oil does not occur below this level of dissolved oxygen.

Conventional laboratory scale experiments have many advantages as they provide well controlled tests conditions and are easily replicated. However, there are certain inherent disadvantages to these small scale systems when operating in either the batch or continuous mode. Microbiologically, wall effects are magnified by the high wall to water ratio, the inability to achieve significant dilution effects or concentration gradients in small volumes of water. The ocean as an environment does not make possible controlled or easily replicated experiments. A compromise meso-scale test system was designed for use in this project with raw seawater.

Experiments were performed to determine the nature and variability of the meso-scale system. Two tanks were filled with seawater from

Fig. 8.6 Oxygen Depletion Rates of S. La Crude, Corexit 9527 and S. La. Crude + Corexit 9527.



Narragansett Bay and water samples removed from 1.5 meters below the surface on days, 0, 4 and 8 for use as inoculum for oxygen depletion studies. Three series were set up in duplicate to define the capacity of the resident population for utilization of endogenous nutrients (control), petroleum (Kuwait) and "total" heterotrophic potential (peptone). The experiment was repeated three times and a composite of the north and south tank data used to perform a polynomial regression for each substrate and the control. From the regression data, the R^2 value was determined and the best fit of the R^2 value to either a second or third degree polynomial. This was used to plot the x value, which is time in days against the estimated y value which is the mg of O_2 /liter at each data point.

The statistical evaluation of the control values (Fig. 8.7) indicates a close correlation for the estimated depletion rates at each of the samples times. This is particularly true of the values for the 0 and 4 day samples. The general trend is for low initial depletion rates of 1.25 and 1.5 mg O_2 /liter/day, followed by essentially level values, then increased oxygen content in the test values. The data indicates rapid exhaustion of the endogenous nutrients which are normally low in seawater.

The data for Kuwait crude oil (Fig. 8.8) shows a close correlation for all sampling times and a consistent oxygen depletion rate over the entire time course of the test. The initial rate is somewhat higher for the 0 day water than for the other two water samples.

A similar plot for "total" heterotrophic potential (Fig. 8.9) demonstrates the highest oxygen depletion rate of the three test series and an extremely close fit for all samples during the first day of the depletion rate measurement. The shifts in rate after one day reflect nutrient depletion and toxic products as seen in the conventional bacterial growth curve.

A comparison of the oxygen depletion rates with oil and peptone by 0 day water from the north and south tanks (Fig. 8.10) demonstrates the close fit of data from two different test tanks. The rates match those obtained from the composite data for all points on the three experiment statistical study.

The VPC method was also used to establish the reproducibility of the meso-scale system. This first validation was performed with only seawater (no oil or dispersant added) and compared to the VPC values of Narragansett Bay water. Samples were taken from 1.5 foot level and 9.5 foot level in both the north and south tanks. The results (Fig. 8.11) show excellent reproducibility between the two tanks and the bay water counts.

Salinity of the tanks was measured at surface, 1.5, 9.5 and 18 foot level (Fig. 8.12). A rain during the first 24 hours significantly reduced the salinity at the tank surface, but did not affect salinity at the other levels in the tank and had no effect on bacterial numbers (Fig. 8.11).

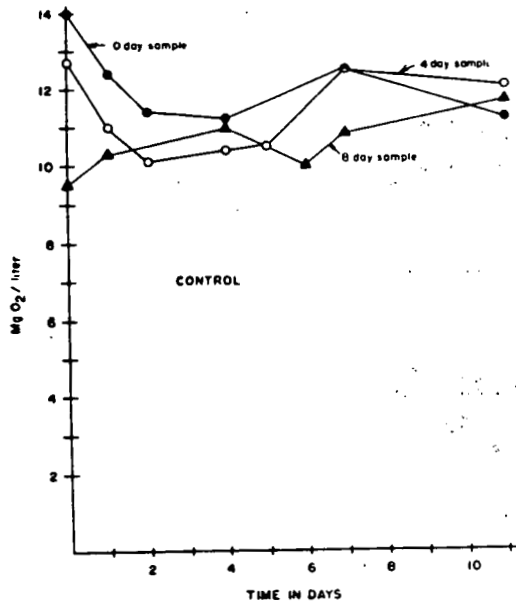


Fig. 8.7 Oxygen Depletion Rates of Zero, Four and Eight Day Control Task Samples.

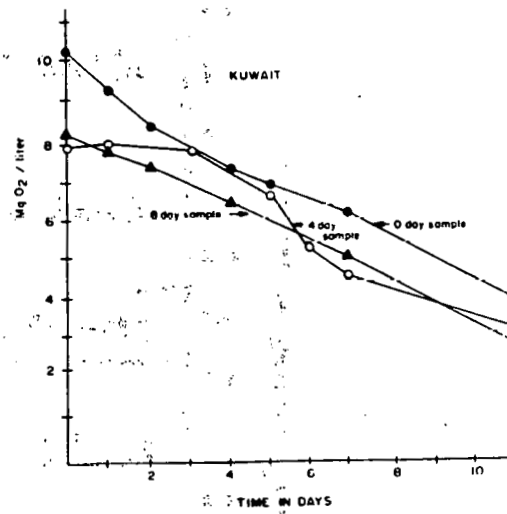


Fig. 8.8 Oxygen Depletion Rates of Zero, Four and Eight Day Kuwait Crude Oil Tank Samples.

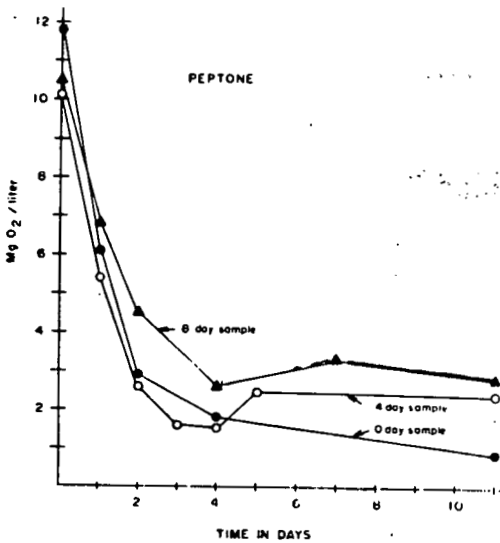


Fig. 8.9 Total Heterotrophic Potential of Zero, Four and Eight Day Samples.

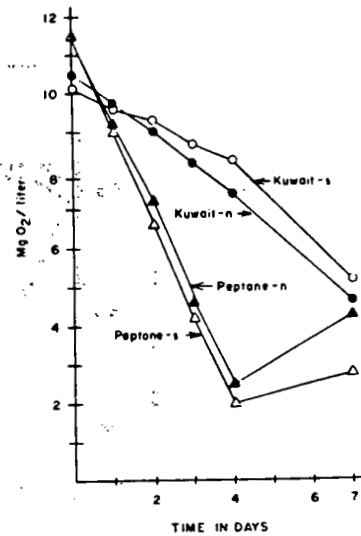


Fig. 8.10 Comparison of Oxygen Depletion Rates of Kuwait with Peptone.

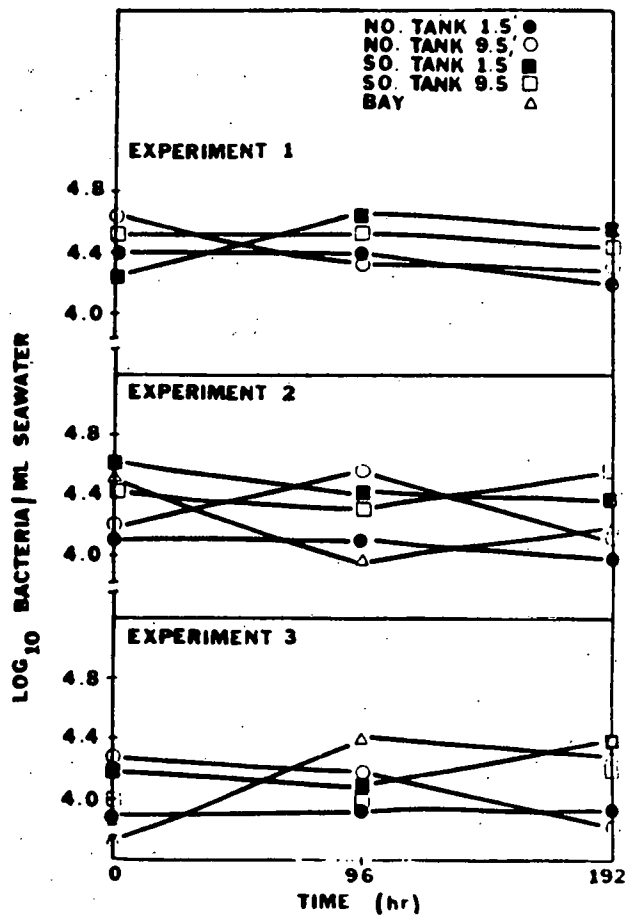


Fig. 8.11 Viable Plate Counts Validations of Test Tanks.

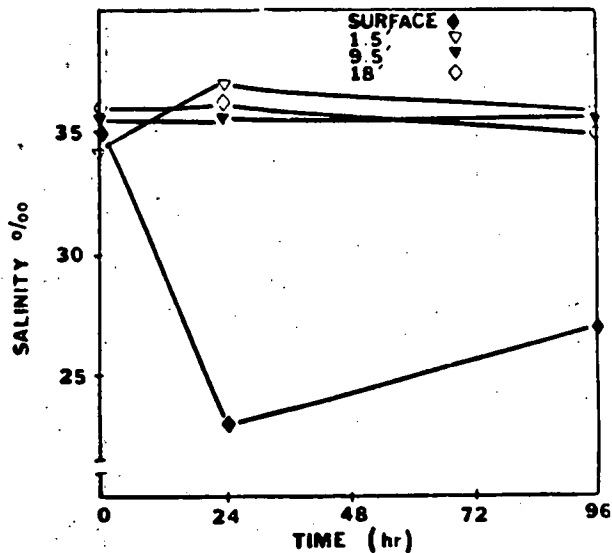


Fig. 8.12 Salinity Concentrations in the North Tank During Meso-Scale Experiment 1.

The reliability of viable plate count (VPC) and most probable number (MPN) data from the same test series is shown in Table 8.2. These values represent the numerical average of the same data points for three replicate experiments. There is a close correlation between the MPN and VPC values within a given tank as well as inter-tank values for the same sample times. The differences in values do not exceed one log and in most cases are much closer. As normally found in MPN and VPC, comparisons of bacterial numbers the MPN values are the higher of the two. These results were supported by carefully controlled laboratory experiments Figure 8.2.

TABLE 8.2 RELIABILITY OF VPC AND MPN DATA FROM MESO-SCALE TANKS

Determination	Sample day	North Tank	South Tank
MPN	0	$7.0 \times 10^3^*$	1.1×10^5
VPC	0	1.5×10^4	1.7×10^4
MPN	4	1.6×10^4	1.1×10^4
VPC	4	1.4×10^4	2.3×10^4
MPN	8	2.2×10^4	1.3×10^4
VPC	8	8.6×10^3	1.9×10^4

*One test only.

The response of the total heterotrophic population to Kuwait crude oil and Kuwait dispersed with Corexit 9527 was tested in the meso-scale system. The north and south tanks each received 15 ppm of Kuwait and 3 ppm of Corexit 9527 was added to the south tank. The surface of both tanks received mixing (glass rod) for five minutes after chemical additions. Both tanks were sampled at 0, 24, 48 and 72 hours from the 1.5, 9.5 and 18 foot sample spigots. Dilutions from the samples were spread plated on to OZR medium and incubated at tank temperature (21°C) for six days.

The VPC data (Fig. 8.13) demonstrated more than one log increase during the first 24 hours in the dispersant treated tank (south tank), a level value between 24 and 48 hours, followed by a decrease in bacterial numbers at 72 hours. In the north tank, which received only Kuwait crude oil, there is an apparent trend for increased bacterial numbers during the 72 hour test period. The change in bacterial number in the north tank is minor compared to the south tank and may not represent bacterial growth but normal variation seen in VPC determinations. There was good correlation between bacterial numbers in the south tank and essentially the same values at all three test levels, suggesting a homogeneous mixture throughout the tank.

The enhanced growth in the dispersed oil tank could reflect metabolism of oil and/or dispersant. Mulkins-Phillips and Steward (11) in their experiments using gas chromatography to follow changes in components found that the dispersants were metabolized in preference to the C₁₇ - C₂₈ fraction of the Arabian crude oil used in their experiments. In contrast, Atlas and Bartha (12) using mineralization as a

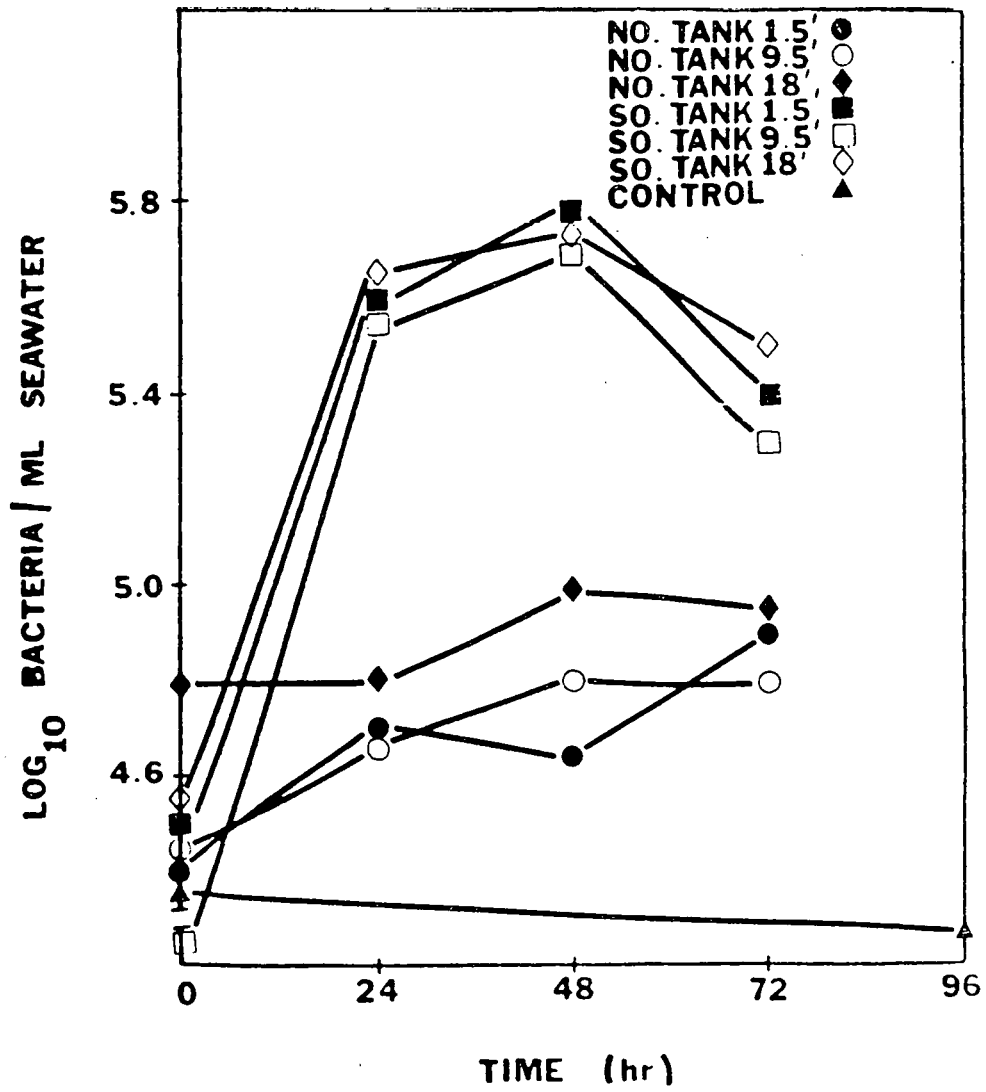


Fig. 8.13 VPC Data of Control, Kuwait Crude, and Kuwait Crude and Dispersant in the Meso-Scale Tanks.

measure of biodegradation, showed that dispersants increased the microbial utilization of Sweden crude oil.

The quantitative chemical analyses of the tanks for extractable organics (Exp. 2 Chemistry Section) demonstrated control values of 210 and 243 ppb in the seawater. The extractable organics in the oil tank are elevated only at the one hour samples taken at the top and mid zones of the tank. After one hour they return to or below background level. This would support the interpretation of no bacterial response in this tank. The quantity of extractable organics in the dispersant treated tank is significant at all levels and would provide sufficient substrate for increase in microbial numbers. The limiting factor, however, would be the quantity of nitrogen and phosphate available rather than carbon. The decrease in bacterial numbers between hours 48 and 72 (Fig. 8.13) are not related to carbon limitation which in all zones of the tank are well in excess of 500 ppb.

The qualitative GLC data from the chemical studies indicates loss of components boiling below $n\text{-C}_{15}$ in the dispersant treated tank. The loss of these components may reflect biodegradation or evaporation or a combination of the two phenomenon and would support the observed increase in microbial numbers.

TABLE 8.3 OXYGEN DEPLETION RATES FROM MESO-SCALE EXPERIMENT 2
OIL AND OIL PLUS COREXIT 9527, mg L^{-1}

DAY	OIL			OIL AND COREXIT 9527		
	TOP	MID	BOT	TOP	MID	BOT
0	1.72	2.32	1.72	1.31	1.34	1.41
1	0.61	1.01	4.45	0.31	1.82	3.23
2	0.52	1.17	1.37	0.63	0.84	0.50
3	0.09	0	-	0.76	0.04	2.09

The oxygen depletion data from this experiment (Table 8.3) is highly confusing and apparently is of little value. The results were erratic except for day 0 results which were rather constant. A trend does exist in the dispersant treated tank which suggests increased activity with time at the lower region of the tank.

The third meso-scale experiment contained several modifications. The third tank was in place and used as a control tank containing only seawater. A cooling system was installed which maintained ambient bay temperature $+ 2^{\circ}\text{C}$. An agitator was installed in the upper 2 feet of the water column and operated eight hours each day. Samples were taken from the 1.5, 9.5 and 18 foot levels at 24 and 48 hours. Samples were plated for both "total" heterotrophic bacteria (THB) and total number hydrocarbonoclastic bacteria (HYB) (Figures 8.14 and 8.15).

The THB counts (Figure 8.14) of bay water were constant over the two days of the experiment. The values in the 1.5 foot zone of the control

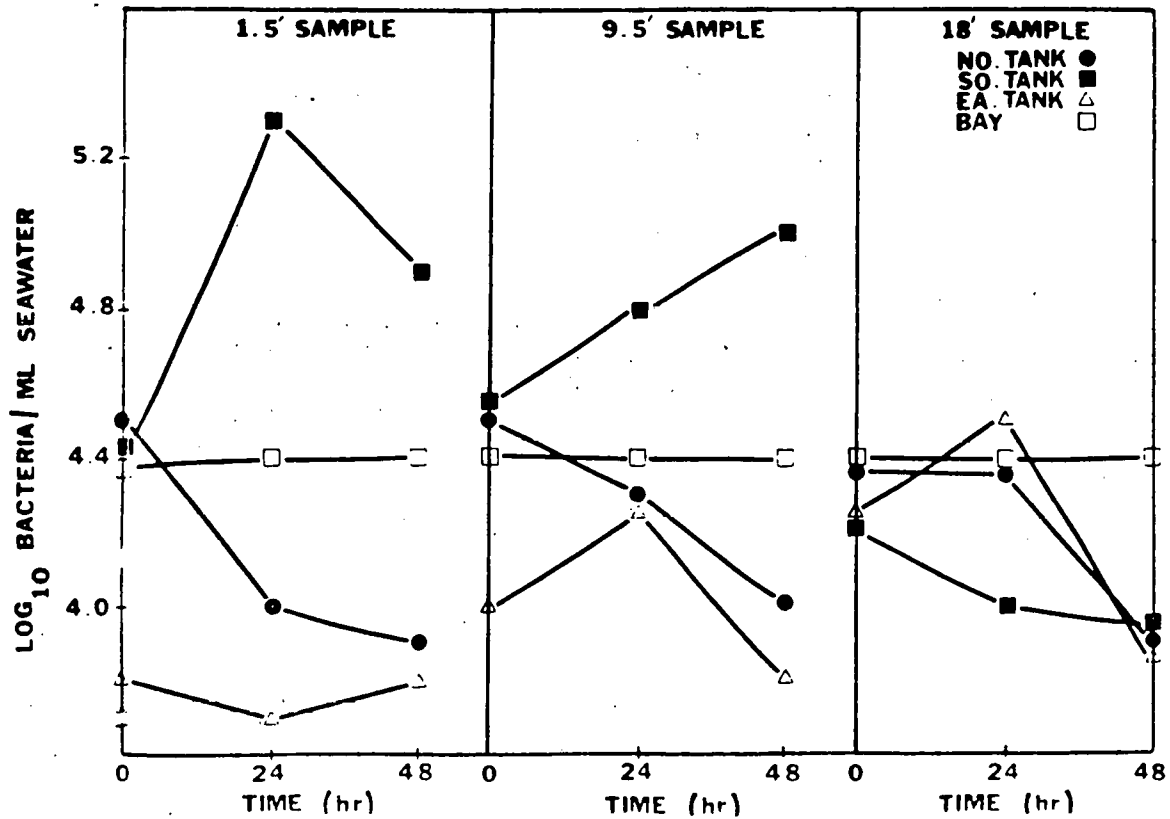


Fig. 8.14 Meso-Scale Experiment 3, Measured Heterotrophic Bacterial Growth.

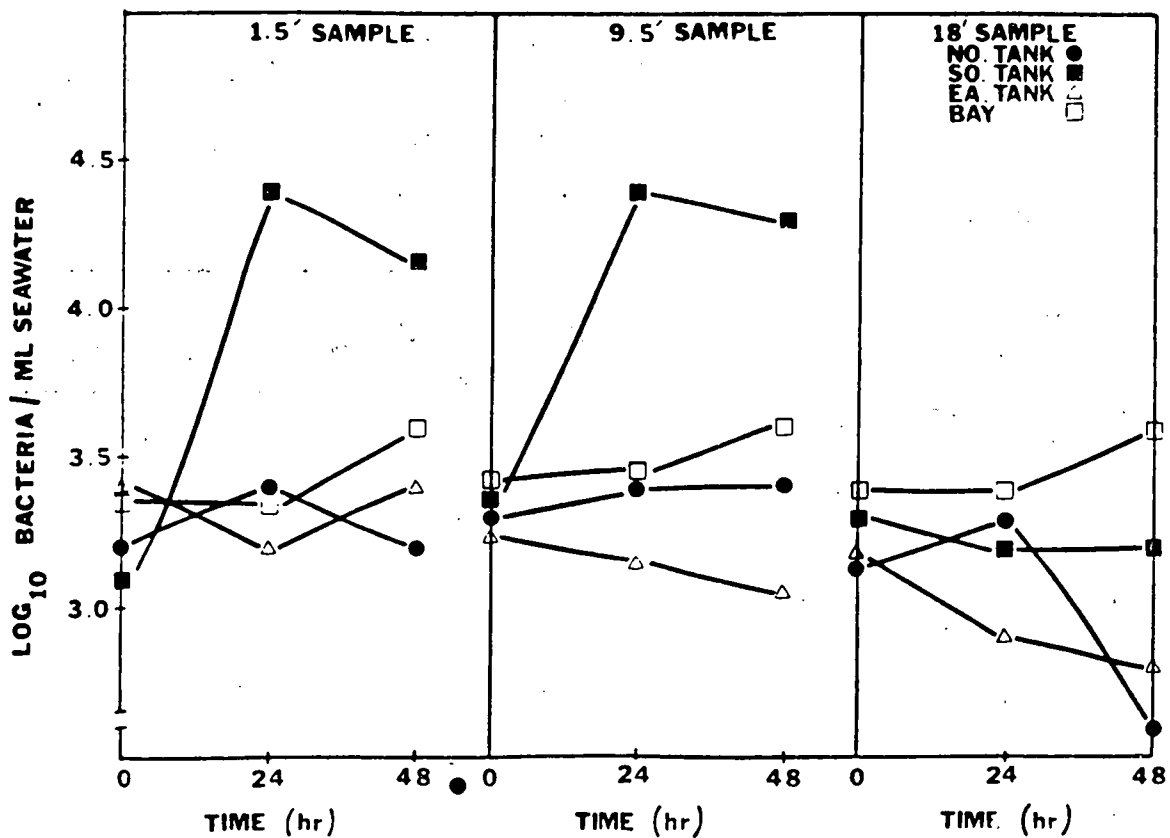


Fig. 8.15 Meso-Scale Experiment 3, Growth of Marine Hydrocarbon Degrading Bacteria.

tank were also constant but somewhat lower than the bay counts. There are apparent increases in THB of the oil plus dispersant tank which peaked at 24 hours at the top zone and 48 hours in the mid zone. However, the number of total heterotrophic bacteria in the bottom zone decayed over the course of 48 hours.

Although the actual numbers were somewhat less the trends for HYB were about the same as the THB counts. There was more stability in the top and mid zone counts which showed no significant change in HYB.

There appears to be a relationship between the number of hydrocarbon utilizing bacteria (HYB) and extractable organics in the water column. In the top and mid zones there are increased HYB present in the water column following the appearance of oil in a particular zone of the tank. For example, in the top zone hour 1 samples (chemistry data experiment 3) the oil concentration increased from about 450 ppb to nearly 2000 ppb between hours 1 and 24, and the HYB population also increased during this period. In the bottom zone the oil concentration never reached 900 ppb and there was no change in the HYB population. It might be inferred from this data that a critical oil concentration in the water is necessary for selection of hydrocarbon utilizing bacteria. Unfortunately, we cannot make the same comparison from the second experiment because we measured only THB.

Oxygen depletion measurements (Figures 8.16-8.23) essentially confirm the plate count and chemistry data. The initial biological activity was highest in the top zone of the oil-dispersant tank, somewhat decreased after 24 hours and had returned to baseline (control tank), rates by 48 hours. There is evidence of very little biological activity in the tank dosed with Kuwait crude oil. The bottom samples demonstrated no significant biological activity in the 0 and day 1 samples of either the oil or oil-dispersant tank. There is measurable activity in the oil-dispersant tank samples on days 2 and 3.

It was apparent from these two experiments that dispersed oil does induce slight increases in the total heterotrophic bacterial population (THB) and the hydrocarbonoclastic bacterial population (HYB). These effects were not as apparent as the results of the laboratory experiments of other investigators (11,12) in which the system was supplemented by the addition of nitrogen and phosphorus which are nutrient limiting in seawater.

Experiments were designed to determine the effects of oil and dispersant on bacterial population dynamics. These were small tank experiments under controlled laboratory conditions at 4°C with sediment and seawater collected from Narragansett Bay. All tanks were gently shaken at 45 rpm and aerated to insure sufficient oxygen for maintenance of biological activity. The test series were: control seawater-sediment; Kuwait crude oil 15 ppm (v/v); Kuwait crude oil 15 ppm (v/v) plus 3 ppm (v/v) of Corexit 9527; and Corexit 9527 3 ppm (v/v). Samples were taken from the surface of the tanks (film area), mid water column and the sediments. Each sample was diluted and plated in duplicate onto OZR medium to express the heterotrophic bacterial population. Countable plates (30-300 colonies) were selected from each sample source to serve as

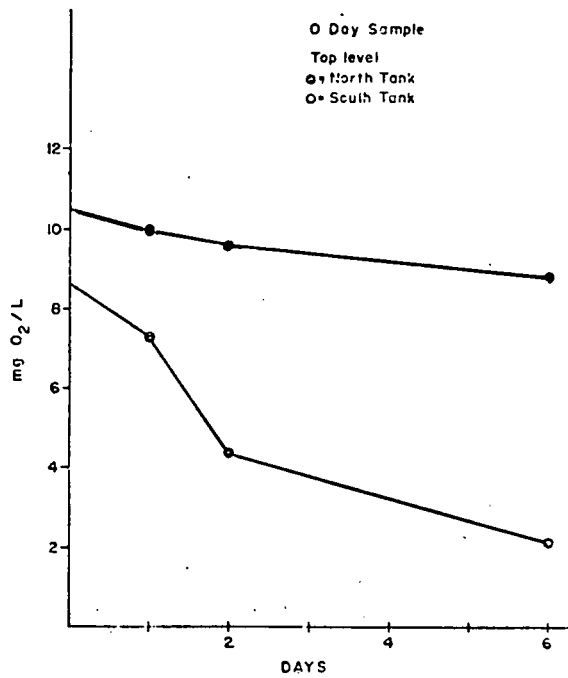


Fig. 8.16 Oxygen Depletion by Kuwait (North Tank) and Kuwait plus Corexit 9527 - Zero-Day Sample.

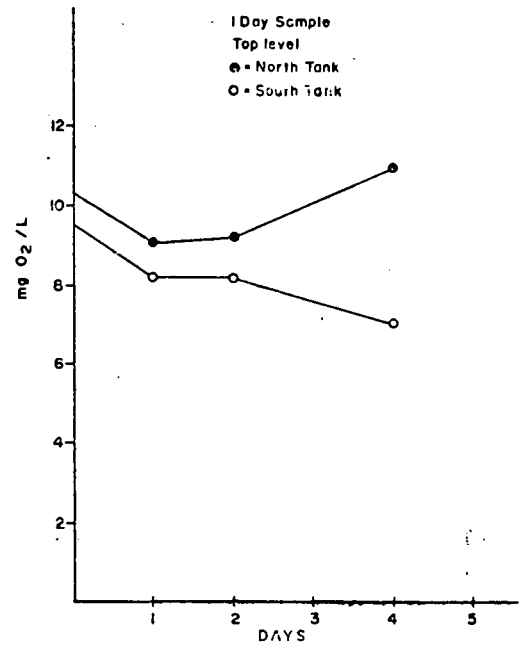


Fig. 8.17 Oxygen Depletion by Kuwait (North Tank) and Kuwait Plus Corexit 9527, One Day Sample. Top Level.

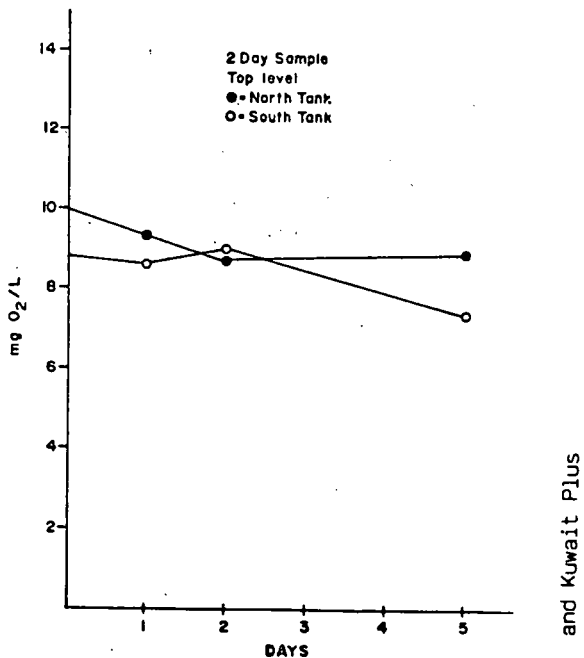


Fig. 8.18 Oxygen depletion by Kuwait (North Tank) and Kuwait Plus Corexit 9527 - Two Day Sample. Top Level.

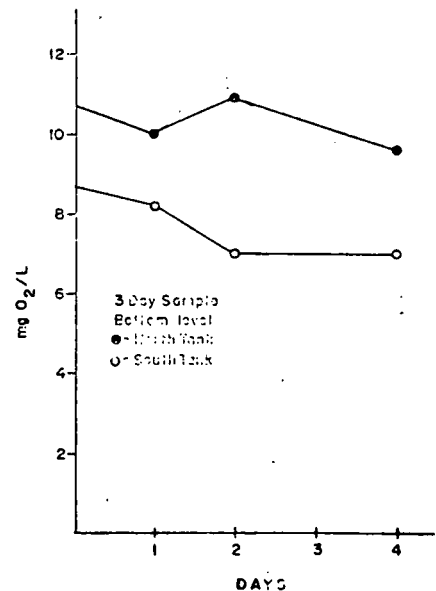


Fig. 8.19 Oxygen Depletion by Kuwait (North Tank) Corexit 9527 - Three Day Sample. Bottom Level.

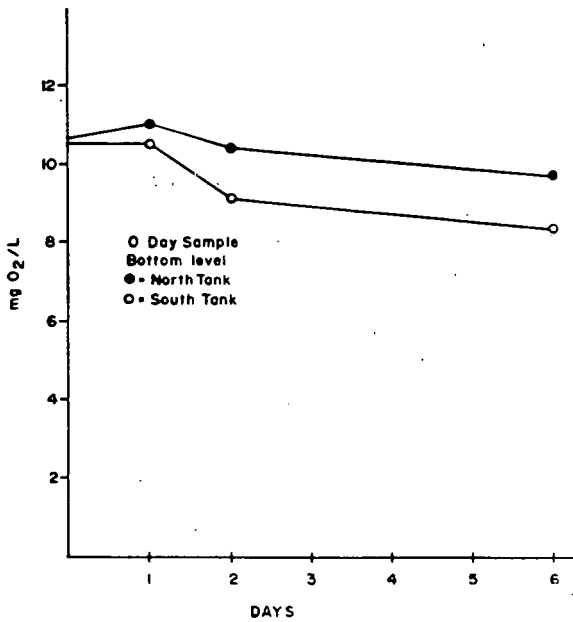


Fig. 8.20 Oxygen Depletion by Kuwait (North Tank) and Kuwait Plus Corexit 9527 - Zero Day Sample. Bottom Level.

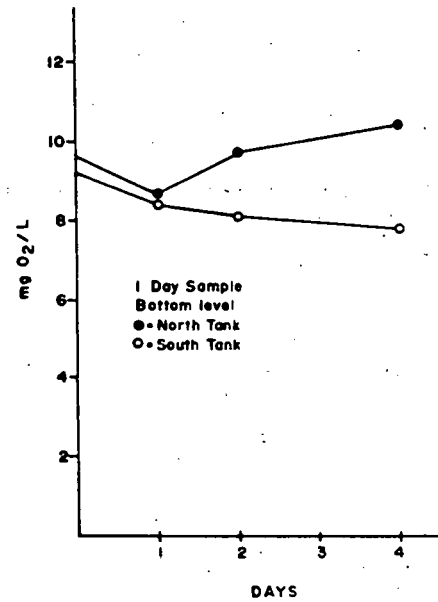


Fig. 8.21 Oxygen Depletion by Kuwait (North Tank) and Kuwait Plus Corexit - 9527 One Day Sample. Bottom Level.

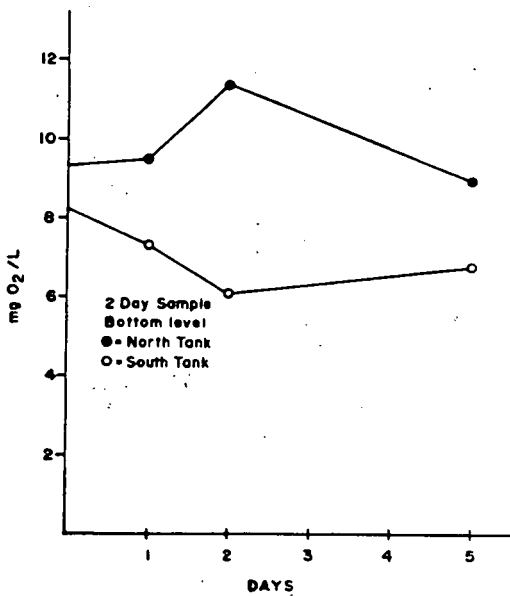


Fig. 8.22 Oxygen Depletion by Kuwait (North Tank) and Kuwait Plus Corexit - 9527 Two Day Sample. Bottom Level.

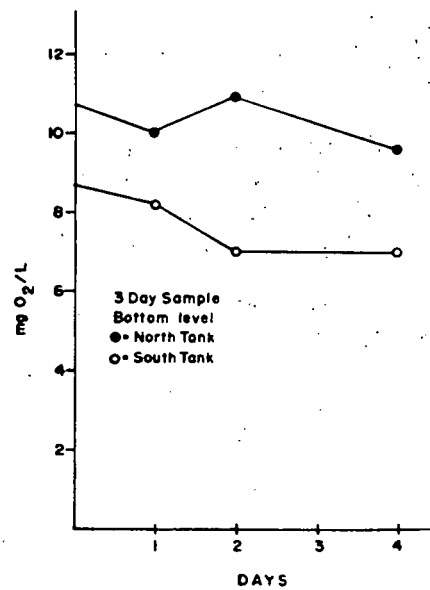


Fig. 8.23 Oxygen Depletion by Kuwait (North Tank) and Kuwait Plus Corexit - 9527 Three Day Sample. Bottom Level.

master plates for replication. The master plates were replicated to n-hexadecane, naphthalene, Kuwait and basal agars. All replicate and master plates were photographed in color for examination of colony types and verification of visual comparison made prior to photography.

The water column series included a Kuwait crude oil MPN series and duplicate sets of OZR plates incubated at 4°C and 13°C. The temperature differential test was performed to see if the system contained a mixture of psychrophilic and mesophilic bacteria which has been demonstrated to occur in Narragansett Bay (13,14).

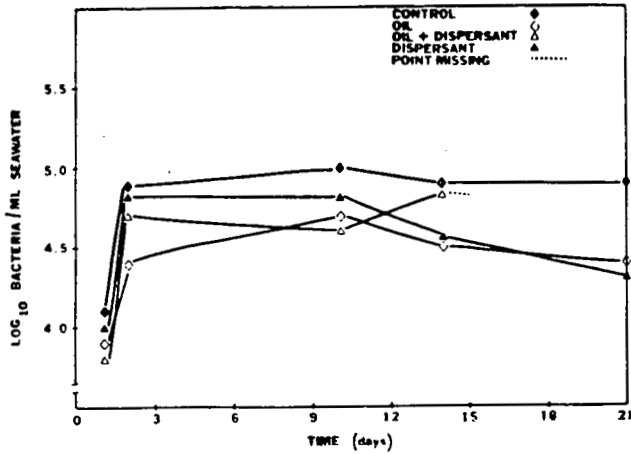
The VPC data for the surface films, sediment and water column at 13 and 4°C are shown in Figures 8.24 a-d. There was an increase in bacterial numbers of the surface film between day 1 and 2 in all four tanks. The least increase was in the oil tank which of course has an oil film at the air-water interface. The oil film was expected to destroy the function of the interface microlayer which typically shows considerable enrichment of bacteria and bacterial nutrients as compared to the water column. Indeed these increases in bacterial numbers could be interpreted as the forming of the microlayer rather than growth of bacteria. This hypothesis is supported by the organism increase in the control tank. The population size in all the surface samples does remain essentially constant through the 21 day experiment.

There are greater fluctuations in the sediment VPC data in all tanks. A general trend is apparent for an increase in the sediment bacterial population through day nine in the control, dispersant and oil-dispersant tanks. There is less of a trend for sediment enrichment in the oil tank. After day nine sediment numbers decline in the control and dispersant tanks but remain stable in the oil and oil-dispersant tanks.

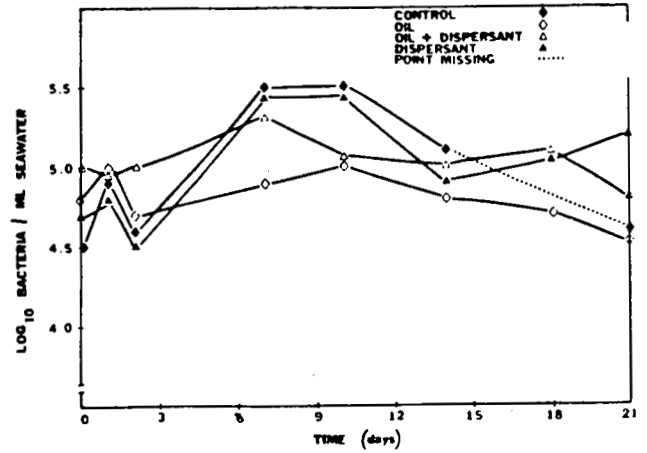
The water column studies at 4 and 13°C are interesting in that they demonstrate evidence for two different populations, each with somewhat different dynamics. The initial 13°C population is larger than the 4°C population in the water column. There is a slight positive trend for the 13°C population through day 14 then a significant decline except in the control tank. On the other hand, the initial 4°C population is low in all tanks but rapidly increases by day three and then more slowly through day seven in all tanks. This is followed by a significant population decline, except in the control tank, through day 14.

The numbers of HYB in the water column were determined by the VPC and MPN methods (Figure 8.25). As normally found in comparison of the two methods, the MPN values are higher than VPC values. This is partially explained by the fact that the two methods select for different heterotrophic populations (15).

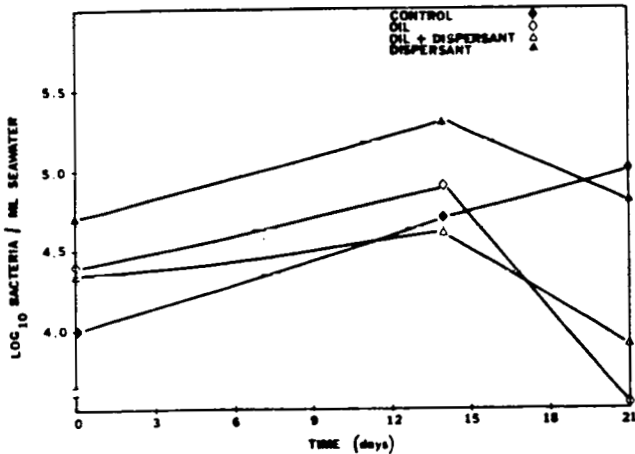
In all the tanks using both the hydrocarbonoclastic MPN and VPC methods, there was a rapid increase in the number of HYB in all tanks until about day 7 after which the numbers declined to initial numbers found in the various tanks. The decline is less rapid by the MPN method but probably would have returned to baseline by days 18-20. We believe the decline is related to exhaustion of the N, P and Fe content of this closed system.



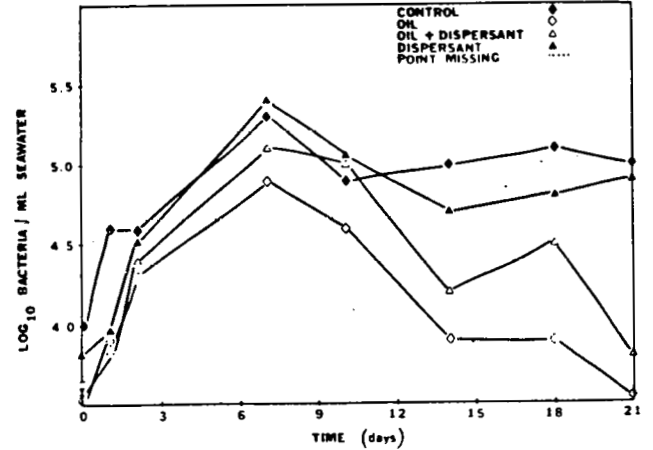
8.24 A Surface Samples



8.24 B Sediment Samples



8.24 C Water Column Samples at 13°C Incubation Temperature



8.24 D Water Column Samples at 40°C Incubation Temperature

Fig. 8.24 Laboratory Experiment, Viable Plate Counts on OZR Medium from Surface

(A), sediment (B), and water column samples (C). Water column samples were incubated at 13°C and 4°C (D). Samples were taken from four aquaria with Narragansett Bay water plus: (1) control, (2) Kuwait crude oil 15 ppm (v/v), (3) Kuwait crude oil 15 ppm (v/v) plus 3 ppm (v/v) of dispersant Corexit 9527, and (4) Corexit 9527 3 ppm (v/v)

It should be pointed out that this system received mechanical agitation which provides a rather uniform distribution of material throughout the water column as compared to the meso-scale tanks. Also the ambient temperature of the bay water and sediment used in this experiment was 10°C so that the 40°C incubations more nearly track bay conditions. It is significant that a sizeable population can be obtained at 130°C incubation.

The diversity of the heterotrophic bacterial population was tabulated by counting the number of each type of colony on each of the OZR master plates from the surface film, water column and sediment samples. Colony morphology types and descriptions are given in Appendix I. The data indicate that the colony diversity decreased during the course of the experiment, with 2 or 3 colony types becoming predominant over the 21 day time frame of this experiment. The decrease in colony diversity occurred to a greater extent in the water column and surface film than in sediments.

In order to simplify the expression of colony diversity two methods were employed in analyzing the data from Appendix 2. In Fig. 8.26 colony diversity was expressed as the change in the number of colony types occurring on OZR master plates over time. The data depicts the decline in the number of colony types with time in the aquarium system. The other method of simplifying the expression of colony diversity was to quantify the degree of dominance within the total heterotrophic population of each OZR master plate.

Dominance was quantified by the equation $c = (n_i/N)^2$ where c the dominance factor is equal to the square of the ratio n_i the number of colonies of each colony type divided by N the number of colony types (100). The larger the value of c the greater is the predominance of bacterial species within the given population. The results are given in Fig. 8.27. The relationship between Fig. 8.26, the degree of dominance, and Fig. 8.24, the change in total heterotrophic bacterial numbers, suggests that the increase in bacterial numbers in all four aquaria was accomplished by a few bacterial species that predominated in the stressed environment of the aquaria system.

The degree of change in the heterotrophic bacterial population demonstrated a similar trend in all four aquaria. The data indicates that the aquaria system used was responsible for the changes in the bacterial populations and that the system used exerted a greater stress on the heterotrophic population than did the Kuwait crude oil and/or Corexit 9527. These findings are in concurrence with results published by Kaster and Van Auken (75). Kaster and Van Auken examined bacterial populations from the surface waters of the Gulf of Mexico over an eight week period. In their experiment South Louisiana Crude oil (0.5%) was added to one flask system and another flask served as a control. Over the eight week period there was an increase in bacterial numbers but a decrease in the bacterial diversity in both flasks. No significant difference in the heterotrophic bacterial population was detectable between the oiled flask and the control flask.

The replica plating data in Appendix 2 was incorporated with the data on the diversity of the heterotrophic bacterial population because the

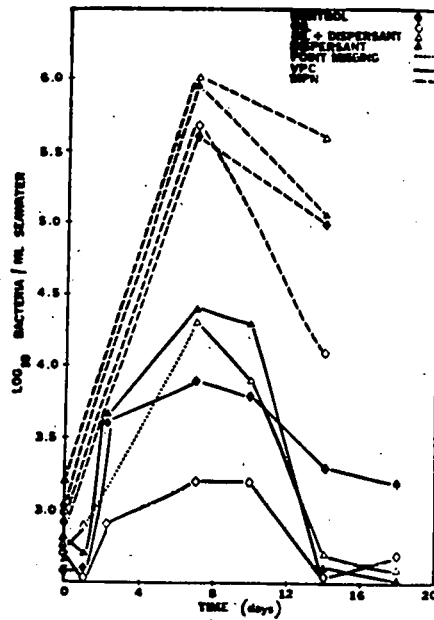


Fig. 8.25 Laboratory Experiment, Viable Plate Counts (VPC) and Most Probable Numbers (MPN) with Kuwait Crude Medium.

(MPN) with Kuwait Crude medium incubated at 4°C were processed from water column samples. Four aquaria with Narragansett Bay water plus: (1) control, (2) Kuwait crude oil 15 ppm (v/v), (3) Corexit 9527, 3 ppm (v/v), and (4) Corexit 9527 3ppm (v/v). (MPN data points one day seven for the control and oil tanks were 5.6+, meaning the real value is greater than 5.6 but of an unknown amount.)

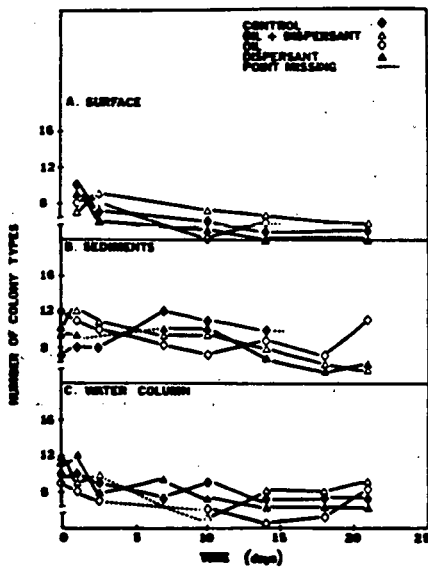


Fig. 8.26 Colony Diversity Expressed as Number of Colony Types over Time

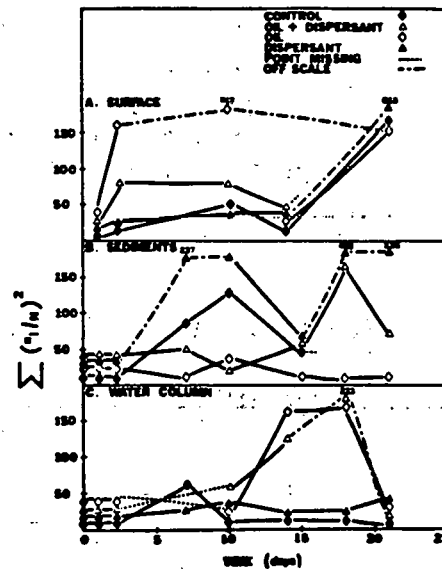


Fig. 8.27 Colony Diversity Expressed as Quantification of Dominance

Fig. 8.26 and 8.27. Colony diversity of heterotrophic bacterial population on OZR master plates from surface, water column, and sediment samples. Narragansett Bay water plus: (1) control, (2) Kuwait crude oil 15 ppm (v/v), (3) Kuwait crude oil 15 ppm (v/v) + 3 ppm (v/v) of the dispersant Corexit 9527, and (4) Corexit 9527 3 ppm (v/v). The heterotrophic diversity is expressed as: (1) the total number of colony types on OZR master plates and (2) by the degree of dominance given by $C = \sum (n_i/N)^2$, where n_i equals the number of colonies of each colony type and N equals the total number of colony types.

oil degrading bacteria grew on both the OZR master plates and the hydrocarbon replica plates. The data suggests that no enrichment for hydrocarbon degraders occurred in the aquarium system as was originally anticipated. Table 8.4 exemplifies the data on the presence of hydrocarbon degraders during the time of the laboratory experiment. In Table 8.4 the number and type of hydrocarbon degraders are given from the Kuwait crude aquarium. The data exemplifies the low numbers and random nature of the presence of oil degraders in the aquarium system. The lack of enrichment may have been due in part to the stress of the aquarium system as mentioned previously and the cold temperature (4°C) of the seawater. The hydrocarbon metabolizing bacterial isolates usually metabolized only one of the hydrocarbon substrates with only a few being able to metabolize two or three substrates. The lack of predominance by any bacterial hydrocarbon utilizing species, as determined by colony diversity suggests that the different fractions of the Kuwait crude were simultaneously metabolized. Simultaneous metabolism is further substantiated by the even distribution of bacterial colonies growing on the different hydrocarbon substrates. Zobell (145) suggested that simultaneous metabolism of oil would occur under low substrate conditions. The aquarium system with 15 ppm (v/v) of Kuwait crude oil at 4°C would have very little oil in the water column due to the low solubility of Kuwait crude at this low temperature. The dispersant was probably inefficient in dispersing the oil in the aquarium system because of the low volumes applied, the difficulties of properly applying the small volume of dispersant, and because the oil often became stuck to the sides of the aquarium and the glassware making it unavailable for mixing with the seawater and dispersant.

Table 8.4 Hydrocarbon utilizers in heterotrophic bacterial population as determined by replica plating. Samples were taken from the Kuwait crude aquarium in the laboratory experiment. Colony types are given in Appendix 1.

Hydrocarbon Utilizers							
Day	Kuwait Crude		Hexadecane		Naphthalene		Total #
	Colony type	#	Colony type	#	Colony type	#	
0	19	4	16	2			
			23	1	15	2	9
1	19	1					
	3	1		0		0	4
	1	2					
2	19	1					
	25	1		0		0	2
7		0	4	4		0	4
14	19	1		0		0	1
18		0		0		0	0
21	19	3					
	3	2	4	1	15	2	8

A long term experiment was designed to develop an approach for conversion to a flow-thru test system. The test system utilized four 55

gallon microcosms structured as diagrammed in Figure 8.28. Fresh seawater from the Jerusalem station, where the tests were performed, was introduced to the microcosms via a jet system which established a circular subsurface flow pattern in the top portion of the microcosms. The water was removed from the bottom zone so that flow was from the top reaction zone to the tank bottom where the test scallops were located. These systems all contained a sediment base obtained from the water adjacent to the Jerusalem test facility.

The Data Input-Output of this experiment is summarized in Table 8.5.

Table 8.5 Data Input-Output, Jerusalem Flow-Thru System,
5/7/79 - 7/2/79

Control TMB	Oil TMB	Dispersant TMB	Oil-Dispersant TMB
INPUT			Output
1.			no ml ⁻¹
2.			no ml ⁻¹
3.			ppb
4.			ng hr ⁻¹
5.			weeks
6.			ng hr ⁻¹
7.			weeks
8.			hours
9.			°C
10.			ppt
11.			ug ml ⁻¹
12.			uM
13.			Recorder plot
14.			No. dead
15.			No. Swimming Claps

The data collected in the experiment is presented in computer entry format (Table 8.6). This data was analyzed by multiple regression and other techniques.

Multiple step-wise regression analysis of the data on this long term (5/7/79 - 6/25/80) experiment indicated no significant correlations between a number of the experimental parameters. A 0.5000 significance level was established for entry into the model.

There were no significant correlations between total hydrocarbon concentration and day of sampling or samples from top, middle or bottom portions of the flow-thru tanks. The tank temperatures increased from a low of 10.6°C to a high of 18.7°C over the course of the 50 day experiment but showed no correlation to total heterotrophic bacteria, total hydrocarbonoclastic bacteria, or hydrocarbon mineralization rates. A positive correlation was not found between total hydrocarbon concentration in the water column and either hexadecane or naphthalene mineralization rates. There was, however, a negative relationship when mean values (Table 8.7) were examined indicating inhibition of mineralization rates

Table 8.7 Mean Values from the Jerusalem Flow Thru Tests

Tank	No. Bact x 10 ³ Hetero	Hydrocarb	Hexadec* mineral ng/hr.	Hexadec* T/f weeks	Naph* mineral ng/hr.	Naph* T/f weeks	Total Hydrocar ppb	Total mineral rate	D/f, hrs. Total hydro- carbon
Control	5.3	2.8	11.99	373	19.58	205	107	(31.48)	3.4
Oil	6.2	4.1	10.25	342	8.34	253	279	(18.59)	15.0
Dispersant	3.5	2.5	9.84	275	16.72	261	1534	(26.56)	57.8
Oil and Dispersant	8.2	6.3	8.62	344	11.09	193	475	(19.71)	9.8

*Tested against μ /mg substrate

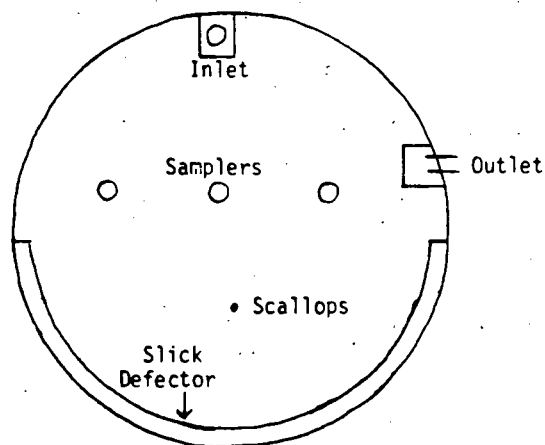
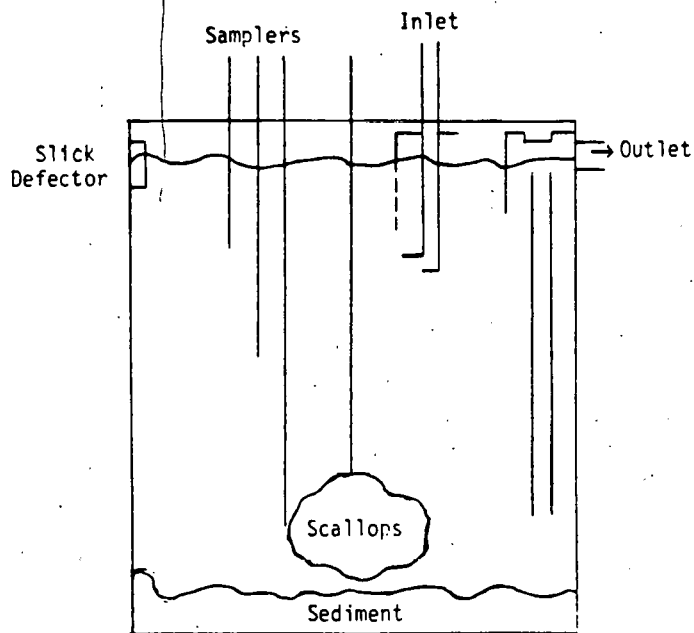


Figure 8.28 Test System for 55 Gallon Microcosm Flow Thru Experiment

in the presence of higher concentrations of hydrocarbon or dispersant. This observation cannot be explained with the existing data.

There was a significant correlation between the number of total heterotrophic and total hydrocarbonoclastic bacteria in the various test tanks. The numbers of hydrocarbonoclastic bacteria were always lower than total heterotrophic bacteria, but approach unity in the oil and dispersant treated tanks (1.3) and are further from unity in the seawater control tank (1.8). These data do indicate selection for hydrocarbonoclastic bacteria in tanks containing oil and/or dispersant.

There was a decrease in hydrocarbon turnover time in the oil and/or dispersant tanks which is most apparent for turn over of aliphatic hydrocarbons whereas the effect is less apparent for aromatic hydrocarbons. Generally, however, aromatic hydrocarbons are mineralized more effectively than the aliphatic constituents. It must be noted, however, that the aromatic hydrocarbons turned over in this series represent lower molecular material than the turned over aliphatic material that was turned over.

Since the actual mineralization rates show little variation the degradation time in a particular situation becomes primarily a function of hydrocarbon concentration. It now becomes apparent that degradation potential is a fairly constant value in the marine environment. The changes in temperature, salinity phosphate and ammonia nitrogen are more apparent than real. For example, the highest phosphate and ammonia values are limiting for the amount of carbon in the environment and hence do not manifest a measurable effect upon the test parameters. The temperature span was only 8.1°C which is significantly below the 10°C span for a Q_{10} value of 2 normally expected. However, it has been shown previously (Traxler and Cundell, 1975) that the Q_{10} values for hydrocarbon utilization in marine systems vary between 1.3 and 1.8. Therefore with the 8.1°C span we would not expect to measure a significant temperature effect. Salinity changes were not significant for bacterial activity.

Four meso-scale tank experiments were performed in May, June and July 1980 to compare two dispersants, Corexit 9527 and BP 1100WD. In experiment 1 (5/19 - 5/23) the two test tanks (N and S) were dosed with 120 ml of Kuwait crude oil and 6 ml of Corexit 9527. The oil and dispersant were premixed at the test site and applied to the top of the water column. The agitators were run for an 8 hour on, 16 hour off cycle for the 5 day test period. Experiments 2, 3 and 4 were conducted as a direct comparison of the two dispersants. The north tank contained 120 ml of Kuwait crude oil plus 6 ml of Corexit 9527 while the south tank was dosed with 120 ml of Kuwait crude oil and 6 ml of BP 1100WD. Water samples were collected from the top port located in the mixing zone and from the outlet port for bottom samples.

Hydrocarbon analyses were performed using a quantitative gas chromatography method (Butler and Levy, 1978) which involved 12 hour continuous liquid-liquid extraction of the samples with n-pentane followed by a 12 hour extraction with benzene. These extracts were desulfured by passing through copper shavings, concentrated by flash evaporation and placed on a silica gel over alumina column. The alkanes were eluted with n-pentane

and the aromatics with benzene. Both fractions were concentrated to 0.5 ml and 2 ul injected onto the proper column with a predetermined temperature program for chromatography. Samples were spiked with a known quantity of pristane and anthracene prior to extraction (internal standards) and all determinations were computer integrated against the internal standards. External standards were determined using the same quantity of pristane and anthracene for calculation of extraction efficiency. This method provided the concentration of total aliphatics in ppb and total aromatics in ppb. Addition of these two values provided total hydrocarbon in ppb.

Quantitative gas chromatography was used to determine the total peak area of Corexit 9527 in the water stock solutions used in the scallop experiments presented in Section 9 of this report. This value was then converted to mg l^{-1} as oil and subtracted from the integrated total hydrocarbon in the oil dispersant mixture. The results of these quantitative determinations are shown in Table 8.8. These results show ratios of oil to dispersant identical to those determined by the infra-red method (Table 4.5.4 this report).

Microbiological activity was measured in the mixing zone of all tanks and degradative activity determined as mineralization rate for total hydrocarbon using hexadecane, naphthalene and benzo (a) pyrene as representative hydrocarbons. These were used to spike 50 ul of Kuwait crude oil in their ratio present in the oil (1.0:0.5:0.1). The challenge was against the test tank microflora in 3 hour determinations.

The quantitative data for hydrocarbon concentration in the meso-scale tanks are summarized in Tables 8.9-8.12. The amount of oil in the untreated seawater ranged from 103-121 ppb except for one determination thought to be contaminated in the laboratory extraction process. Dispersant carried considerable oil into the water at the mixing zone during day one. Elevated levels of oil remained in the mixing zone during the course of all experiments. The values varied from experiment to experiment but generally were found to be in thousands of ppb. The ratio of aliphatic to aromatic hydrocarbon also varied in the various samples and different experiments.

In these experiments, there was little oil carried to the bottom of the test tanks, the values being 2 to 3 times the control water values but manifold less than the mixing zone values. These experiments confirm earlier data which suggest essentially the same phenomenon of dilution through the water column. Both dispersants (Corexit and BP) respond alike in the entrainment of oil in the mixing zone and dilution through the water column. The toxicity tests to scallops are discussed in the biology section and indicate no effect at these measured concentrations of oil. The scallops from the control tank were combined and extracted as a unit then analyzed for hydrocarbon content. The composite of the test scallops were also analyzed in the same fashion.

The result of oil analyses on the scallops (Table 8.9-8.12) show identical low values (6ppb) in experiment 1, slightly elevated levels in the BP 1100WD treated scallops in experiment 2 and 3 but still well below anticipated toxicity values. These animals were exposed to oil levels well above those detected in the animals. The data suggests that the scallops do not accumulate oil.

Table 8.8 Hydrocarbon Concentration in Behavioral Test Stock Solutions

Stock Solution	Hydrocarbon mg/Liter		
	Aromatic	Aliphatic	Total
Kuwait Crude Oil	26.34	18.28	44.62
Corexit 9527	19.54	13.88	33.42
Kuwait Crude Oil Plus Corexit 9527	39.14	20.78	59.92
Oil in Mixture	19.60	6.9	26.5

Table 8.9 Experiment 1:
Hydrocarbon Content of Water and Scallop Samples

Date	Tank	ppb Aliphatic	ppb Aromatic	ppb Hydrocarbon
5/19	ST	269	340	609
	SB	27	180	207
5/21	ST	-	-	-
	SB	173	148	321
5/22	ST	1647	126	1773
	SB	-	-	-
5/19	NT	1009	429	1438
	NB	69	lost	lost
5/21	NT	633	533	1166
	NB	-	-	-
5/22	NT	GC Abort	40	-
	NB	-	-	-
5/19	CT	64	52	116
	CB	1	5	6
5/23	Cont. Scallops	2	4	6
5/23	Test Scallops	4	2	6

N and S tanks were dosed with 120 ml oil and 6 ml Corexit 9527 (1:20) premixed. Agitator used. Extraction efficiency 91%.

Table 8.10
Experiment 2. Hydrocarbon Content of Water and Scallop Samples

Date	Tank	ppb Aliphatic	ppb Aromatic	ppb Hydrocarbon
6/3	ST	280	560	840
	NT	4,500	1,760	6,260
	CT	10	93	103
6/4	ST	13,000	2,300	15,300
	NT	9,040	760	9,800
	CT	460	88	548
6/5	ST	2,280	500	2,780
	SB	53	70	123
	NB	2,552	18	2,570
	CB	15	-	-
6/6	ST	22,780	1,520	24,300
	NT	4,100	500	4,600
6/9	ST	1,696	520	2,216
	SB	21	178	199
	NT	640	1,760	2,400
	NB	16	-	-
	CT	40	30	70
6/9	Cont Scallops	5	14	19
	S Scallops	6	26	32
	N Scallops	2	14	16

N Tank dosed 120 ml oil and 6 ml Corexit 9527

S Tank dosed 120 ml oil and 6 ml BP 1100 WD

Oil and dispersants premixed. Agitator used. Extraction efficiency 96%.

Table 8.11
Experiment 3: Hydrocarbon Content of Water and Scallop Samples

DATE	Tank	ppb Aliphatic	ppb Aromatic	ppb Hydrocarbon
6/16	ST	180	1480	1660
	NT	60	2840	2900
	NB	6	21	27
6/17	NT	180	399	579
6/18	NB	6	50	56
6/19	ST	100	2040	2140
	NT	20	4540	4560
6/20	ST	40	1000	1040
	NT	180	500	680
	CB	8	113	121
6/19	Scallops Con	8	89	97
	Scallops N	9	1	10
	Scallops S	4	82	86

N tank dosed 120 ml Kuwait and 6 ml Corexit 9527. S tank dosed 120 ml Kuwait and 6 ml BP 1100 WD.

Table 8.12
Experiment 4. Hydrocarbon Content of Water and Scallop Samples

Date	Tank	ppb Aliphatic	ppb Aromatic	ppb Hydrocarbon
7/7	ST	140	400	540
	NT	200	500	700
	NB	8	-	-
7/8	ST	60	640	700
	NT	40	1680	1720
	CT	60	640	700
7/9	ST	-	20	-
	SB	-	1.25	-
	NT	40	20	60
7/11	ST	60	20	80
	NT	-	66	-
	NB	1.25	1.25	2.5
7/11	Scallops N	1	104	105
	Scallops S	-	78	-
	Scallops Cont	88	28	116

N Tank dosed 120 ml Kuwait and 6 ml Corexit 9527
S Tank dosed 120 ml Kuwait and 6 ml BP 1100 WD.

The biodegradation data is summarized in Table 8.13. Calculation of turnover time was based on recovered radioactivity and is expressed as $T/f \cdot R$ in hours. In these experiments, we measured not only mineralization but also the hydrocarbon converted to low molecular weight water soluble products and alcohol soluble products. This is a more accurate measurement of degradative potential than mineralization alone. We challenged the microbial populations with a constant quantity of substrate oil (50 μ l) which eliminates the tank variable of oil concentration and allows full expression of the potential. The organisms in the control tank yield constant $T/f \cdot R$ values of approximately 7 hours. This is the time required to completely turnover a standard amount (55.8 ng) of the challenge ^{14}C hydrocarbon mixture. This factor is therefore a measure of biological activity against a fixed amount of substrate and can be used to estimate the degradation potential or time required to degrade the amount of oil in the sample. We find by inspection of the data that there is not much variation in the oil concentrations in the different samples.

The results obtained in this study indicate that the introduction of oil or dispersed oil into seawater does not invoke a significant change in the size of the heterotrophic bacterial population in seawater. There is a change in the percentage of hydrocarbonoclastic bacteria within the heterotrophic population indicative of a natural selection for organisms able to metabolize hydrocarbon components. This modified population does have a slightly greater potential for hydrocarbon utilization, but in terms of the vastly increased hydrocarbon content, little overall enhanced significance in relation to degradation time. The reason for this limited microbial response to oil in the water column is, of course, the nutrient limited nature of seawater in terms of its nitrogen, phosphorus and iron content. Active cell growth and maximum rates of nutrient turnover (hydrocarbon in this case) will not occur in a nutrient limited system. This study has demonstrated that the modest increase in the size of the hydrocarbonoclastic bacterial population, as a result of oil entrainment in the water column, does not have a profound effect on degradation potential.

An explanation for the above observations is the recently proposed hypothesis for bacterial dormancy in aquatic systems (Stevenson, 1978). It is proposed that dormancy is an important physiological adaptation for the survival of bacterial suspended in the water column and for this case, is termed exogenous dormancy in which development is delayed due to some unfavorable chemical or physical condition of the environment. The "dormant cells" are generally small and ovoid as demonstrated by Anderson and Hefferman (1965) and Wright (1973) and functionally turned-off. This need not imply no activity but a state below maximum potential in a satisfactory environment. It appears that this phenomenon could function in the water column to a greater extent than in sediments or the micro-layer where nutrient enrichment occurs.

An obvious approach to increased degradation potential is nutrient supplementation. Oleophilic nitrogen, phosphorus and iron supplements have been proposed to stimulate bacterial growth in marine water column populations. A tank experiment was performed to test the response of bacterial populations to supplemented vs. non-supplemented Kuwait-Corexit mixtures in seawater. The results are summarized in Table 8.14. The bacterial population size deteriorated with time in the seawater control

Table 8.13
Experiment 1. Total Hydrocarbon Concentration and
Degradation Potential of Meso-Scale Experiments

Test Tank	Test Time Hrs.	T/f R (Hrs)	Total Hydrocarbon ppb	Degradation Potential (Hrs)
Control Seawater	24	6.93	116	14.4
Kuwait and Corexit	24	16.66	1024	305
Control Seawater	72	7.22	116	15
Kuwait and Corexit 9527	72	7.84	1773	249

Experiment 2

Test Tank	Test Time Hrs	T/f R (Hrs)	Hydrocarbon ppb	Degradation Potential Hrs.
Control Seawater	48	6.93	103	12.6
Kuwait and BP 1100 WD	48	22.89	15,300	6276
Kuwait and Corexit 9527	48	6.17	9800	1083
Kuwait and BP 1100 WD	168	274.7	2216	10,909
Kuwait and Corexit 9527	168	126.3	2400	5432

Experiment 3
Test Tank

Control Seawater	48	6.93	109	13.5
Kuwait Corexit 9527	48	9.68	579	100
Kuwait + BP 1100	48	12.08	1660	359
Kuwait + Corexit 9527	120	10.28	680	125
Kuwait BP 1100 WD	120	9.27	1040	172

Experiment 4

Control Seawater	48	6.93	109	13.5
Kuwait Corexit (N)	48	6.86	1680	206
Kuwait BP 1100 WD	48	8.52	640	97
Kuwait Corexit	120	13.72	60	14.8
Kuwait + BP	120	13.42	80	19.2

*T/f.R determined for a total of 55.8 ppb of 14C-hydrocarbons.

Table 8.14 Heterotrophic Bacteria in Nutrient vs.
Non-Nutrient Supplemented Tanks

Time (Hrs)	Seawater Control	Unsupplemented Kuwait & Corexit	N & P Supplemented Kuwait & Corexit
0	1.3×10^5	1.1×10^6	2.4×10^6
24	2.7×10^5	3.0×10^4	1.9×10^7
48	5.0×10^5	2.0×10^4	1.9×10^8

and unsupplemented test tanks. In the nitrogen and phosphate supplemented tank there was a definite increase in total heterotrophic bacteria. Examination of colony types further demonstrated a definite selection for hydrocarbanoclastic bacteria in the enhanced population of the nutrient supplemented tank. Significantly increasing the size of the hydrocarbanoclastic population via an active growth response would be expected to also increase the hydrocarbon turnover rate and expedite degradation.

It is important to sound a warning which needs to be tested under environmental conditions. The process of disease is a quantitative inter-relationship between the number of bacteria, virulence of the bacteria and host resistance as expressed by the formula:

$$D = \frac{NV}{R}$$

In the normal marine environment the sea creatures evolve to a delicate balance between these three factors. If we upset this balance, disease could result with far more damaging consequences to the marine fauna than the described toxicity of oil and/or dispersant. This is strongly supported by the work of Stinson and Talburt (1978) who showed a 3-log increase in virulence of hydrocarbon grown Pseudomonas aeruginosa over that of the same strain grown on glucose. This virulence was linked with the development of a new lipo-protein in the outer membrane of the hexadecane grown cells. Therefore, we must conclude that as tempting as fertilization might be as a mechanism to increase degradation potential, it must be tested under controlled conditions to determine whether or not pathogenicity does result from the increased bacterial numbers.

8.4 Conclusions

Both the viable plate count (VPC) and most probable number (MPN) methods were suitable for enumeration of marine heterotrophic bacteria and hydrocarbanoclastic bacteria.

The MPN method while yielding slightly higher total numbers than the VPC method had no greater accuracy than the VPC method, imposed greater logistical demands and did not yield colonies which were required for other aspects of the project.

Use of these methods demonstrated that the percentage of oil degraders within the "total heterotrophic population" increased with exposure time of the "total population" to oil and/or dispersant.

Oxygen depletion by the modified BOD method is a valuable tool which provides a general picture of biological response to materials suspended in the water column. The procedure was used to demonstrate the biodegradable nature of Corexit 9527 and provide a rough index of degradation potential. This method confirmed VPC and chemistry data in the meso-scale tank experiments. Essentially, there is little water column activity in oil treated tanks but biological activity in the tank zones containing elevated hydrocarbon concentrations.

Oxygen depletion has certain limitations, the greatest being that it cannot be directly correlated with actual oil degradation rate or the rate of degradation of specific oil components. An alternate approach is chemical analysis by gas chromatography which has been used in this project. The use of this technique for water column samples, while quantitative for bulk oil has certain limitations for component analysis. It is possible to demonstrate loss of classes of compounds by this method but is too expensive and time consuming for routine degradation rate determinations. The use of ^{14}C labeled hydrocarbons allows a rapid and fairly simple method for measuring mineralization (conversion of organic carbon to carbon dioxide by metabolism) as an index of biodegradation. Representative hydrocarbons provide an estimate for the rate at which the mixed natural population achieve mineralization of aliphatic and aromatic hydrocarbons. The mineralization rate studies demonstrate turnover rates ranging from approximately 20 to 90 mg of substrate per hour. These values compare with results by other investigators in similar systems.

A more accurate approach using ^{14}C methodology is to measure not only mineralization, but also the production of water soluble intermediates which carry the ^{14}C label and the amount of ^{14}C incorporated into cell biomass. The importance of this approach is apparent from the data from one typical experiment. The average disintegration per minute (DPM) in the CO_2 traps were 4.3×10^3 , 3.2×10^4 DPM for the cell bound activity and 7.1×10^4 DPM for the water soluble products. This data shows clearly that mineralization is an index of biological activity but not a reliable quantitative tool for hydrocarbon turnover or degradation time.

Studies by the VPC method for the surface film, water column and sediment were performed as 13 and 40°C. The bacterial numbers increased in the surface film during day 1 and 2 then remained essentially constant throughout the 21 day experiment. We interpret this increase not as bacterial growth per se but rather the formation of the microlayer.

The sediment bacterial population increased through day 9 in the control, dispersant and oil-dispersant tanks but not in the oil tank. The numbers remain constant in the sediment of the oil-dispersant tank after day 9 but decline in the control and dispersant tanks.

Oil destroys the surface microlayer as such because the oil is imposed between the water and air interface, and we believe that hydrocarbon degrading bacteria tend to be carried into the oil film and thus removing them from an active role at the oil-water interface.

The water column studies at 40 and 130°C provide evidence for two different bacterial populations in the natural seawater which was at 10°C. The total heterotrophic populations shift somewhat but the most significant observations is a rapid increase in the number of hydrocarbonoclastic bacteria through day 7 followed by a decline to original numbers, due, we conclude, to exhaustion of the nitrogen, phosphorus and iron content of the seawater.

Studies showed a decline in colony diversity with time in the tank system suggesting enrichment for specific organisms which is supported by

the studies on the ratio of hydrocarbanoclastic to heterotrophic bacteria. Population dominance is more significant than population size which is a fairly constant value.

The long term flow-through experiment showed no significant correlation between the number of total heterotrophic bacteria and hydrocarbon concentration, but a significant correlation was found between total heterotrophic and total hydrocarbanoclastic bacteria which indicated selection for hydrocarbon-utilizing bacteria.

A negative relationship was found between hydrocarbon content and hexadecane or naphthalene mineralization rates, suggesting inhibition of mineralization at high hydrocarbon and/or dispersant values. However, there was a decrease in hydrocarbon turnover time (T/f) in the oil and/or dispersant tanks. This decrease in T/f is more apparent for aliphatic hydrocarbons than for aromatic hydrocarbons.

The variation in mineralization rates is minimal ranging from 8.6 to 11.9 ng/hr for hexadecane and 8.3 to 19.6 ng/hr for naphthalene. Thus, in the determination of degradation time the most important function is hydrocarbon concentration.

Investigation of phosphate and nitrogen in the test systems reveal values which were always nutrient limiting for the amount of degradable carbon available.

It is our conclusion that hydrocarbon degradation potential in nutrient limited seawater is a relatively constant value independent of the presence or absence of oil in the water column. There is selection for hydrocarbanoclastic bacteria with time but their overall degradation activity as a mixed population is not significantly affected by the enrichment process. Preliminary evidence indicates that nutrient supplements (nitrogen, phosphorus and iron) do have a significant effect on the size of the seawater microbial population and yield a rather homogenous population of hydrocarbon utilizing bacteria in the presence of oil.

A brief discussion of nutrient seeding suggests this is not a viable approach to increased hydrocarbon degradation potential. The danger of increased pathogenicity in nutrient enriched oil-water systems is a real possibility which must be more fully investigated.

Natural microbial hydrocarbon degradative processes are active in the water column of dispersed or non-dispersed oil. These processes will eventually lead to the turnover of the biodegradable oil components. The rate at which oil degradation occurs is not materially enhanced by the dispersion process but dispersion of the oil into small micelles (1-2 μm) suspended in the water column does make the oil available to microbial action in the water column. Due to the physical inaccessibility of microorganisms to the bulk of the oil in a heavy slick, dispersion of the oil is an adjunct to the hydrocarbon degradative capacity of a mixed natural marine water column population.

This project has not shed much light on the affect of microbial populations on dispersed oil entrained into sediments or oil solubilized or suspended as sub-micron micelles in surface microlayers. Limited data

from this project indicates that hydrocarbon degradative potentials in sediments and the surface microlayer may be significantly higher than degradative potentials in the water column.

It is our conclusion that future studies of hydrocarbon degradation of dispersed vs. non-dispersed oils in the marine environment should center on the following topics listed in a general order of priority:

1. Degradative potentials in sediments.
2. Degradative potentials in surface microlayers.
3. The possible enhanced pathogenicity of nutrient enriched oil.
4. The degradative potentials at water-ice and sediment-ice interfaces.

9.0 Biological Investigations

Christopher J. Ordzie

Gina Garofalo

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PREFACE

The information from our research efforts is presented in three major sections, each dealing with and answering questions about related but different aspects of the scallop predator-prey system and the impact of oil and dispersant on this system.

In Section (9.1), the actual bioassay experiments are described. Sections (9.2) and (9.3) present our biological investigations and techniques which form a foundation for all of the sublethal bioassay work. In Section 9.4, the response of a simple predator-prey community to oil, dispersant, and oil-dispersant mixtures. Instead of redescribing methods in Section I, reference is made to either Section II or III where techniques are described in full.

9.1 Section I Lethal and Sublethal effects of short term acute doses of Kuwait Crude Oil and a dispersant Corexit 9527 on Bay Scallops, Argopecten irradians (Lamarck) and two predators at different temperatures

ABSTRACT

Investigations of short term acute exposure of bay scallops, Argopecten irradians and two scallop predators, the oyster drill Urosalpinx cinerea and the common starfish Asterias forbesi, to oil, dispersant, and oil-dispersant mixtures (Kuwait Crude Oil and Corexit 9527) suggested that predator and prey have different lethal susceptibilities. Scallops were most sensitive to dispersant and dispersant mixed with oil, starfish were only sensitive to dispersant while the oyster drill seemed unaffected even though all were exposed to dilutions of identically prepared stock solutions. Scallops were least susceptible during winter months and most susceptible at summer temperatures. Treatment had less effect on predators than on scallops at summer temperatures. Sublethal concentrations of dispersant and oil-dispersant mixtures diminished the behavioral ability of scallops to recognize drills and starfish. The degree of effect increased with temperature. Predator detection of prey at the same concentrations was more complex. The feeding response or posturing reflex of starfish was significantly slowed by all treatments. In contrast, drills were unaffected in their recognition of scallop effluent in a choice chamber after treatment.

9.1.1 INTRODUCTION

There have been many recent investigations of lethal (Anderson et al., 1974; Griffin & Calder, 1977; Lee et al., 1977), as well as sublethal (Dicks, 1976; Percy, 1977; Percy & Mullin, 1977) effects of oils on marine invertebrates. Similarly, much attention has been given to the lethal (Portmann & Connor, 1968; Baker & Crapp, 1974; Wilson, 1977) and sublethal (Swedmark et al., 1971; Hagstrom & Lonning, 1977) effects of dispersants alone. In contrast, the comparative effects of oil, dispersant, and oil-dispersant treatments have received less attention (Hargrave & Newcombe, 1973; Avolizi & Nuwayhid, 1974).

This study was concerned with assessment of lethal and sublethal effects of API standard Kuwait Crude Oil and a dispersant, Corexit 9527 on the bay scallop Argopecten irradians (Lamarck) and two scallop predators; the starfish Asterias forbesi (Desor), and the oyster drill Urosalpinx cinerea (Say). Scallops were chosen because they are a commercially important marine species. Young of the year were used because of their high reproductive potential, which makes them important to the continued survival of scallop populations (Russell, 1973). Scallops have a well documented, predator specific, stereotyped escape response (Curtis, 1966; Mackie, 1970; Moore & Trueman, 1971; Thomas & Gruffydd, 1971; Ordzie & Garofalo, 1980a, see also section II) which we used to assess sublethal effects of oil and dispersant because it is easily quantified and is important to scallop survival. The oyster drill Urosalpinx cinerea has recently been found to be an active predator of scallops (Ordzie & Garofalo, 1980b, see also section III) and scallops show a vigorous escape response when confronted with this predatory drill.

Starfish are well known predators of scallops (Galtsoff & Loosanoff, 1939). Both predators are found in the coastal ponds of Rhode Island where large bay scallop beds are abundant.

It is our design to investigate the effects of oil, dispersant, and oil-dispersant mixtures on the bay scallop and two predators at lethal and sublethal levels at various temperatures. Such a study will provide information on the susceptibility of an ecologically important predator-prey system.

9.1.2 METHODS & RESULTS

9.1.3 Lethal Effects

Methods

Bay scallops, Argopecten irradians, oyster drills, Urosalpinx cinerea, starfish, Asterias forbesi, periwinkles, Littorina littorea (Lamarck) and purple sea urchins, Arbacia punctulate (Lamarck) were collected from Point Judith Pond or Ninigret Pond, Rhode Island, by dredging or diving. All test animals were maintained in the laboratory with running, unfiltered, ambient temperature sea water from Point Judith Pond. Temperatures ranged from -1.5° to 24.2°C and salinity ranged from 27 to 32 ‰ during this study.

Bay scallop, and two scallop predators, the starfish and the oyster drill, were exposed to various concentrations of stock solutions of oil, dispersant, and an oil-dispersant mixture. Stock solutions were prepared in three 55 liter all glass aquaria according to the schedule in Table I. The appropriate amount of oil was poured onto 49.5 liter of ambient temperature sea water. The dispersant was sprayed onto the appropriate mixing tanks after four hours later to allow weathering of the oil. These mixing tanks were set in an ambient temperature, running sea water bath for temperature control at the beginning of the mixing period. Each solution was aerated with a Silent Giant diaphragm pump for the first 20 hours and allowed to settle for the last six hours. Solutions were then withdrawn from below the slick with a PVC siphon inserted prior to addition of oil or dispersant.

Dosing solutions were then prepared by mixing the appropriate volume of stock solution with ambient temperature sea water to make a volume of 20 liters. The concentrations used for the scallop, starfish, and drill bioassays are shown in Table II. Each dosing tank was placed into a common, ambient temperature water bath. At this point, animals were added to dosing tanks for six hours. Aeration was provided for the entire dosing period. Five control tanks, each with 20 liters of sea water, were also placed in the water bath. In both scallop and drill bioassays, 20 animals were used in each of the dosing and control tanks. Because of their tendency to crawl out of tanks, it was necessary to cage the drills in a mesh ban to keep them in the dosing solution. Due to the large size of starfish, ten individuals were placed in each dosing tank. Test animals of approximately equal size were used for each replicate to eliminate presumed differences due to size.

Table I. Proportions (liters) of sea water, oil, and dispersant used to make the treatment stock solutions.

Solution	Proportion (liters) of:			Air mix	Settle
	W	O	D		
C	50.0	---	---	20 hours	6 hours
O	49.5	0.5	---	20 hours	6 hours
D	49.5	---	0.1*	20 hours	6 hours
OD	49.5	0.5	0.1*	20 hours	6 hours

*Dispersant was added four hours after the beginning of mixing.

W - Sea water

O - Kuwait Crude Oil

D - Corexit 9527 Dispersant

Table II. Volumes of stock solutions mixed with sea water to make the appropriate dilutions of stock solution used for all bioassay experiments.

Concentration % of stock solution	Amount of stock solution (Liters)	Sea water (Liters)
100	20	0
70	14	6
50	10	10
25	5	15
12.5	2.5	17.5
6.25	1.25	18.75

After the six hour dosing period, test animals from each treatment and concentration were separately placed into respective 40 liter aquaria each independently supplied with running sea water at a flow rate of 30 ml/sec for a depuration period of five days. The number of survivors in each treatment and concentration and control were counted at the end of the five day period. The number of replicates at each temperature for each organism are presented in Table III.

2. Results

Scallop susceptibility to oil during the six hour dosing regime was not evident even at the highest concentration (100% stock solution). Indeed, at all three temperatures (2^o, 10^o, and 20^oC) survivorship in control and oil treatments was high and essentially identical at 100% (Figure 1). Measurement of total extractable hydrocarbon using the infrared spectrophotometric technique with carbon tetrachloride as the extracting solvent, gave values of 1-4 ppm for the water below the slick of the oil stock solution. Solutions containing dispersant could not be reliably measured at the concentrations used, so all values for these solutions were designated as nominal concentrations. Scallop survivorship was significantly decreased in all treatments involving dispersant. As the concentration of dispersant and oil-dispersant stock solution increased, scallop survivorship decreased at all temperatures.

Scallop survivorship was temperature related in dispersant and oil-dispersant treatments. As temperature increased, scallop survivorship decreased (Figure 2 & 3). There was no significant difference in the effect of the dispersant and oil-dispersant treatments on bay scallops. Probit analysis (Figure 4) used to estimate LD₅₀ values and 95% fiducial limits for scallops also revealed that there was no significant difference between LD₅₀ values for dispersant and oil-dispersant treatments at any temperature. There was, however, a strong concentration-temperature interaction. As temperature increased, the concentration of Corexit 9527 required to kill 50% of the scallops decreased. The LD₅₀ was lowest at summer temperatures.

Starfish showed no appreciable change in survivorship in any except dispersant treatments for tests conducted at 15^o and 20^oC (Figure 5). Even when exposed to full strength stock solution at these high temperatures, survivorship of starfish was always better than 50 percent.

It should be noted that starfish in the oil dosing tanks spawned during exposure at 15^oC. Starfish in control tanks spawned a few days later. No spawning was observed during the 20^oC experiment. A further observation on the condition of starfish suggests that animals exposed to dispersant and oil-dispersant were physically stressed. Many starfish from these treatments had everted stomachs. No other starfish from other treatments were found with this condition.

There were no treatment related oyster drill deaths observed during experiments run at 20^oC (Figure 6). Of 480 drills tested, only two died during the experiment. During dosing, drills in the controls and all concentrations of the oil treatment appeared to exhibit normal crawling behavior while drills in all concentrations of the dispersant and oil-dispersant treatments were retracted into their shells.

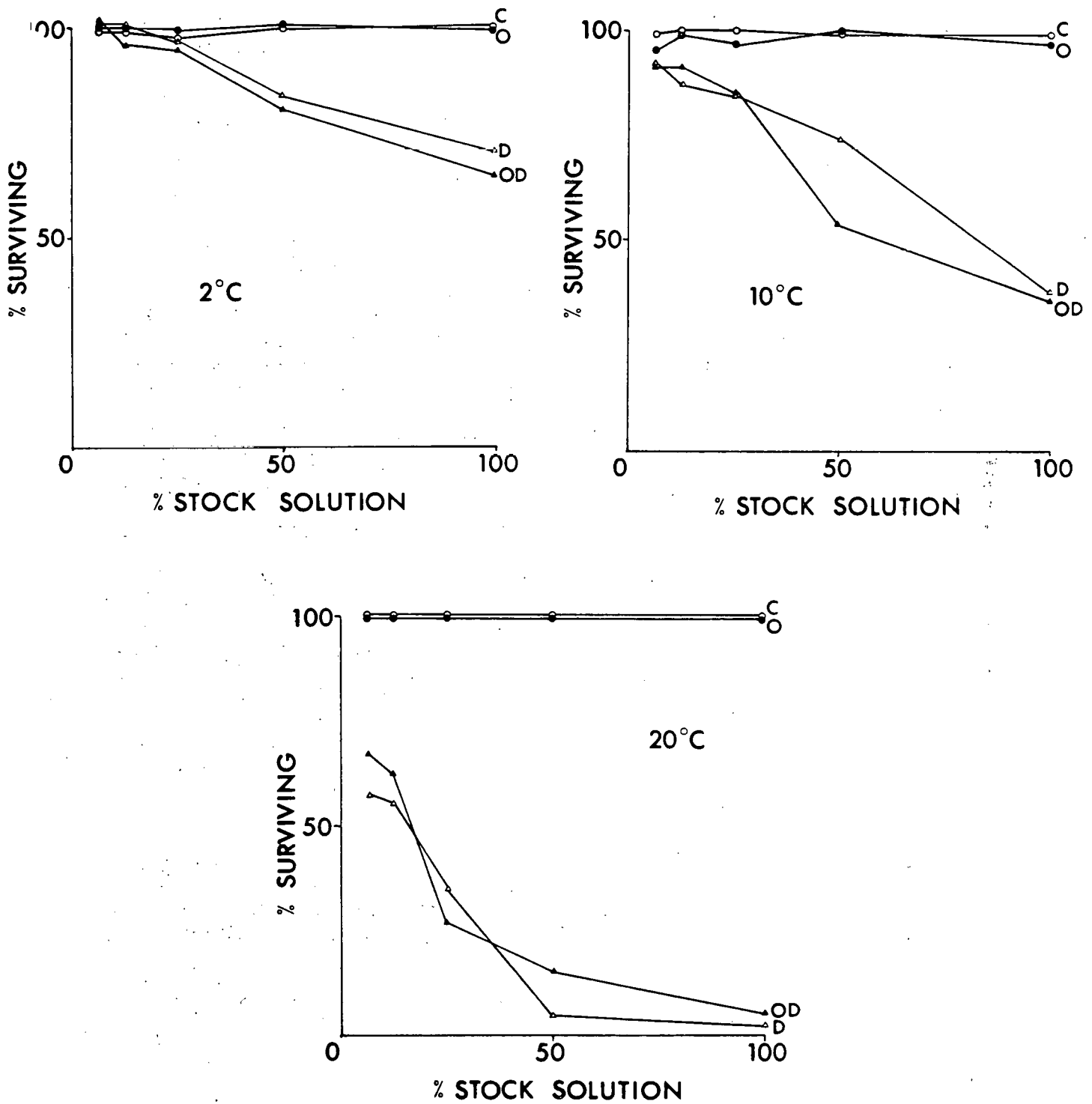


Fig. 1. Scallop survivorship for five concentrations of four treatments at three temperatures, 20, 10, and 2°C: C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

Table III. Temperatures, dates, and organisms used for lethal bioassay.

	Temperature °C	Date	Replicate Number	
Scallops (<i>Argopecten irradians</i>)	20	1/31/78	1	
	20	2/28/78	2	
	20	3/5/79	3	
	20	3/12/79	4	
	100	11/16/77	1	
	100	5/17/78	2	
	100	11/14/78	3	
	100	5/7/79	4	
	200	8/21/78	1	
	200	7/16/79	2	
	Starfish (<i>Asterias forbesi</i>)	150	5/29/79	1
		200	8/6/79	2
Snails (<i>Urosalpinx cinerea</i>)	200	7/23/79	1	
	200	7/30/79	2	

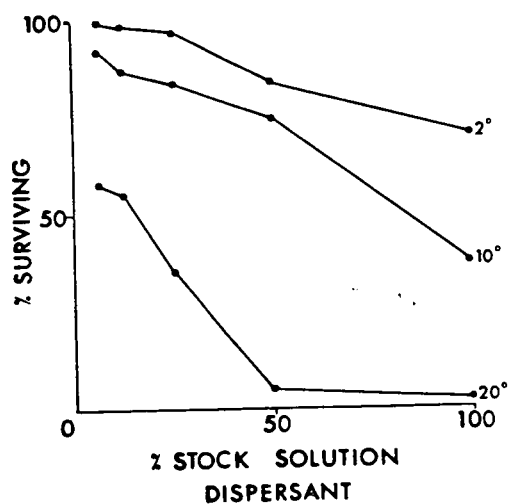


Fig. 2. Scallop Survivorship for five concentrations of dispersant stock solution at three temperatures, 2°, 10°, and 20°C.

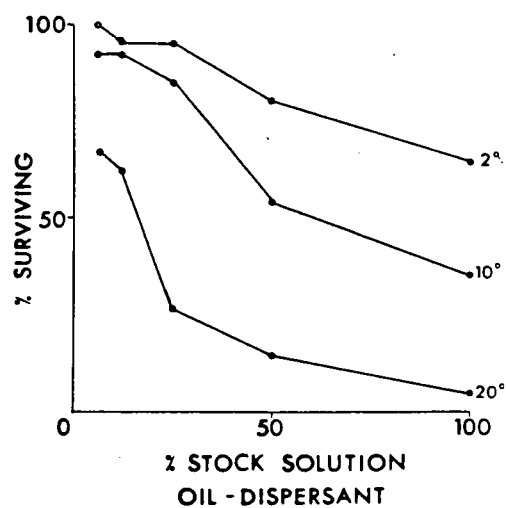


Fig. 3. Scallop survivorship for five concentrations of oil and dispersant stock solution at three temperatures, 2°, 10°, and 20°C.

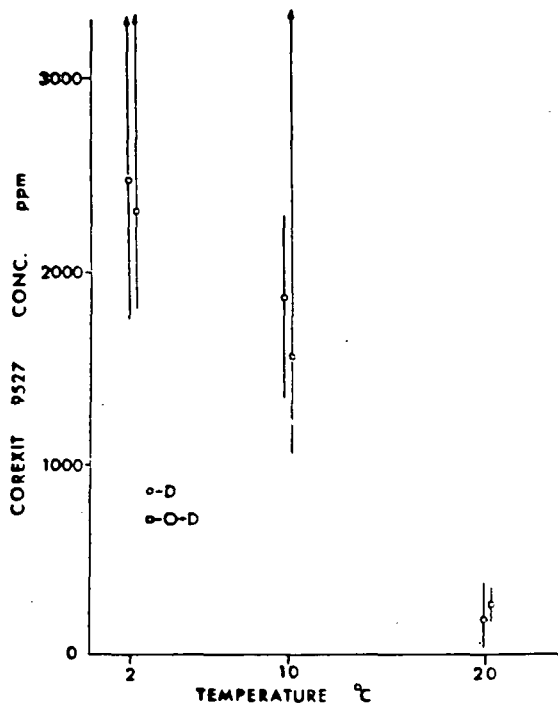


Fig. 4. Probit estimates of 6 hour LC₅₀ for bay scallops at nominal dispersant and oil-dispersant concentrations for 20°, 10°, and 20°C. Vertical lines represent 95% fiducial limits: D-Corexit 9527 Dispersant, OD-Kuwait Crude Oil and Corexit 9527 Dispersant.

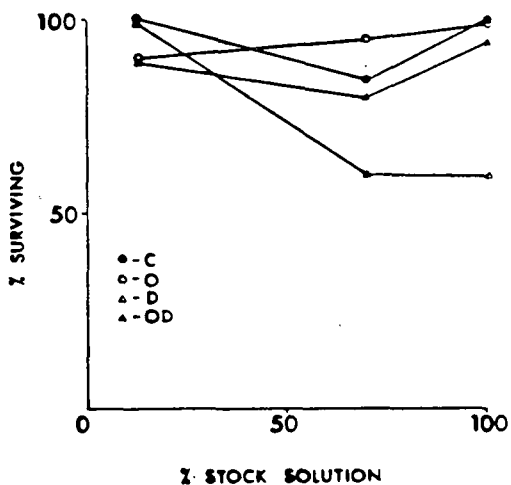


Fig. 5. Combined results of starfish survivorship at 15° and 20°C when exposed to four experimental treatments at various concentrations of stock solution: C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

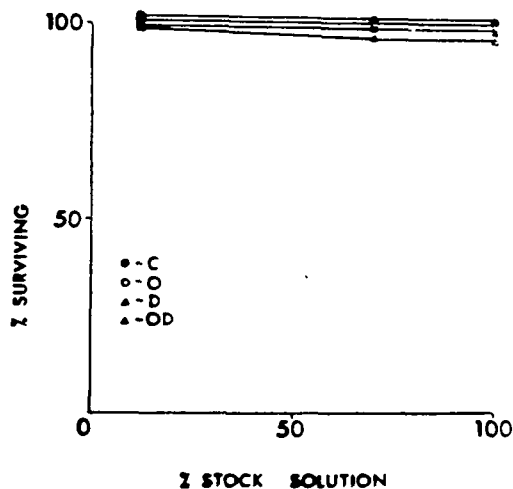


Fig. 6. Oyster Drill survivorship at 20°C when exposed to four experimental treatments at various concentrations of stock solution: C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

9.1.4 Sublethal Effects

1. Scallop Detection of Predators

a. Methods

Scallops from the 12.5% concentration of each treatment and a control were tested for their behavioral recognition of molluscan and echinoderm predators during the five day depuration period which followed dosing. The behavioral escape response and apparatus used were described previously (Ordzie & Garofalo, 1980a, see also section II). Scallops were tested for their behavioral discrimination between a non-predatory gastropod, Littorina littorea and a predatory gastropod, Urosalpinx cinerea. Also, scallop discrimination between a non-predatory echinoderm, Arbacia punctulata and a predatory echinoderm, Asterias forbesi was tested. In each case, the non-predator was presented first to avoid sensitizing scallops.

Scallop stimulation was accomplished by touching the test animal to the scallop mantle margin at the anterior wing. Two aspects of the scallop escape response, response time and swimming claps, were quantified. Response time, defined as the time from beginning of stimulation until first valve movement, was measured in seconds with a stopwatch. Swimming claps were simply counts of the number of valve adductions of closures during a response. It was previously determined that bay scallops respond to predators with a short response time and a high number of swimming claps (Ordzie & Garofalo, 1980a, see also Section II). In contrast, scallops respond to non-predators with long response times and less than one swimming clap. In this way scallops behaviorally discriminate between predators and non-predators. We then studied the effects of oil, dispersant, and oil-dispersant treatments on this sensitive escape response which is so essential to scallop survival.

All 20 scallops from each treatment were tested with non-predator and predator. Each individual scallop was tested five times during the depuration period. Temperatures, replicates, and test species used in sublethal studies are shown in Table IV.

An index was employed to allow simultaneous consideration of scallop responses to predator and non-predator. Response to predator was subtracted from response to non-predator, was divided by their sum, and was then multiplied by 100 as follows:

$$\text{Response Index} = \frac{\text{Non-predator} - \text{Predator}}{\text{Non-predator} + \text{Predator}} \times 100$$

Response time and number of swimming claps were independently analyzed using this index. The index value changes with changes in behavioral discrimination. As behavioral discrimination increases, the index values move away from zero and conversely, as behavioral discrimination decreases, the index values approach zero. Indices for response time and swimming claps were independently analyzed using a two-way analysis of variance test with treatment and temperature as main effects. Data from tests with gastropods and echinoderms were considered separately.

Table IV. Temperatures, dates, and organisms used to test the escape response of treated and untreated scallops.

Tested with <u>L. littorea</u> and <u>U. cinerea</u>		
Temperature	Date	Replicate Number
100	5/17/78	1
100	11/14/78	2
150	6/7/78	1
150	6/18/78	2
200	8/21/78	1
200	7/16/79	2
Tested with <u>A. punctulata</u> and <u>A. forbesi</u>		
Temperature	Date	Replicate Number
100	5/7/79	1
100	5/14/79	2
200	7/23/79	1
200	7/23/79	2

b. Results

Scallop discrimination of Urosalpinx cinerea from Littorina littorea as measured by the time index was significantly decreased by dispersant and oil-dispersant treatments at 12.5% of the stock solution (Figure 7). As temperature increased from 10^o to 20^oC, discrimination increased in all treatments (ANOVA, $F=66.5$, $d.f.=2,468$, $P < .001$). Compared to controls, the oil treatment appeared to have no effect on the scallop response time index. However, dispersant and oil-dispersant treatments both significantly lowered the response time index and thus discrimination (ANOVA, $F=26.4$, $d.f.=3,468$, $P < .001$). There was also a significant temperature-treatment interaction evidenced by the greater effect on discrimination at higher temperatures (ANOVA, $F=2.5$, $d.f.=6,468$, $P < .02$). Scallop behavioral discrimination between the two snails as measured by claps was unaffected by treatment at 10^o and 20^oC (Figure 8). All values were similar to those for controls. The only temperature (ANOVA, $F=20.8$, $d.f.=2,468$, $P < .001$) and treatment effects (ANOVA, $F=5.7$, $d.f.=3,468$, $P < .0009$) were found at 15^oC where all three treatments differed significantly from the control. There was no significant temperature-treatment interaction.

The same indices were used to test scallop discrimination between the starfish, Asterias forbesi and the sea urchin, Arbacia punctulata. Dispersant and oil-dispersant were found to significantly affect the scallop response time index at both 10^o and 20^oC (ANOVA, $F=24.7$, $d.f.=3,312$, $P < .0001$). Scallops were less able to behaviorally discriminate the predatory starfish from the non-predatory sea urchin after exposure to either treatment (Figure 9). There was no temperature effect on discrimination, however, there was a temperature-treatment interaction (ANOVA, $F=2.9$, $d.f.=3,312$, $P < .04$) demonstrated by the greater interference with discrimination at higher temperatures.

The swimming clap index was only affected by the oil treatment at 20^oC and in this case discrimination increased compared to controls (ANOVA, $F=3.79$, $d.f.=3,312$, $P < .01$) (Figure 10). No temperature effect was found, but there was a temperature-treatment interaction (ANOVA, $F=3.08$, $d.f.=3,312$, $P < .03$) owing to increased discrimination of scallops exposed to oil at 20^oC.

2. Predator Detection of Scallops

2.1 Starfish (Asterias forbesi)

a. Methods

Starfish were tested for sublethal behavioral effects using part of the feeding response described as the "posturing reflex" (Heeb, 1973). Starfish "posture" over their prey prior to feeding by elevating their aboral surface which leaves them in a humped posture.

To examine this response an epoxy coated plywood box (30 cm long x 27 cm wide x 13.5 cm deep) fitted with a drain and a glass false bottom was filled with sea water at ambient temperature. A starfish was placed on the glass plate then the water level was adjusted so the water surface just touched the highest part of the aboral surface of the starfish at

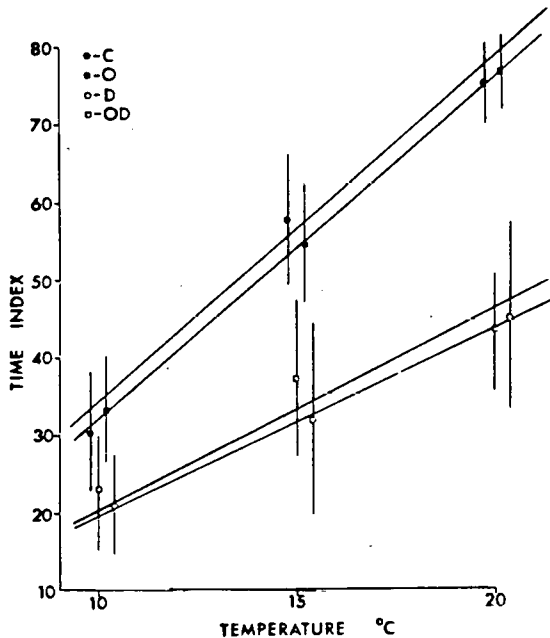


Fig. 7. Response time index for scallop response to *Littorina littorea* and *Urosalpinx cinerea* at each of the four experimental treatments at 10, 15, and 20°C. Vertical lines represent 2 s.e. on either side of the mean. C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

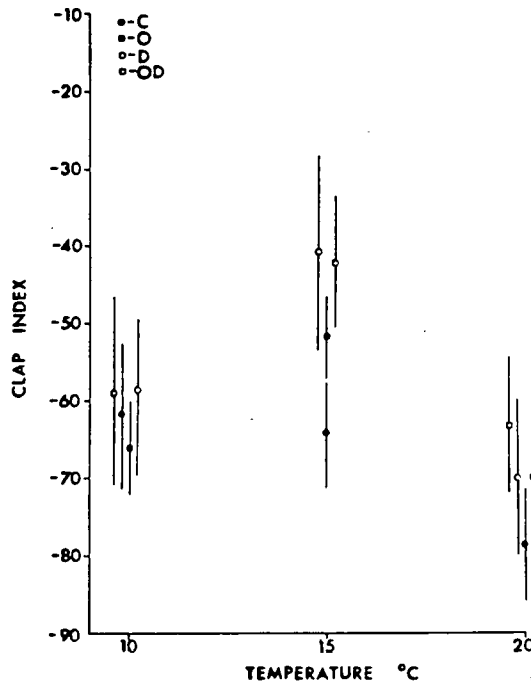


Fig. 8. Swimming clap index for scallop response to *Littorina littorea* and *Urosalpinx cinerea* at each of the four experimental treatments at 10, 15, and 20°C. Vertical lines represent 2 s.e. on either side of the mean. C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

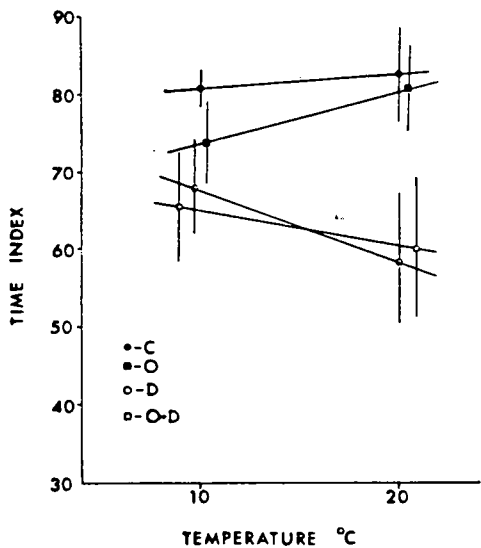


Fig. 9. Response time index for scallop response to *Arctica punctulata* and *Asterias forbesi* at each of the four treatments at 10 and 20°C. Vertical lines represent 2 s.e. on either side of the mean. C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

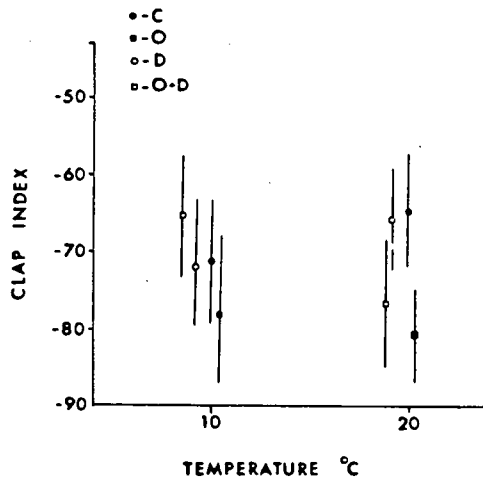


Fig. 10. Swimming clap index for scallop response to *Arctica punctulata* and *Asterias forbesi* at each of the four treatments at 10 and 20°C. Vertical lines represent 2 s.e. on either side of the mean. C-Control, O-Kuwait Crude Oil, D-Corexit 9527 Dispersant, OD-Oil and Dispersant.

rest. Scallop homogenate was made by liquifying tissues from five whole scallops with 15 ml of sea water in a blender. Half a ml of this homogenate was then presented by pipette under the oral surface to stimulate the posturing reflex. The time from initial stimulation to the first upward movement, noted when the aboral surface broke the water-air interface, was measured in seconds up to a 60 second cutoff time. The box was flushed with sea water after each test. Each starfish from the 12.5% concentration of all treatments and control were tested in this manner eight times during the five day depuration period. Plain sea water was also presented by pipette to control for mechanical stimulation of the oral surface in 20 starfish. This experiment was performed at 15°C (5/29/79) and 20°C (8/6/79). Data were analyzed with a one-way analysis of variance test.

b. Results

Combined data from replicates 1 and 2 (15°C and 20°C) respectively (Table V), showed that response times for initiation of the posturing reflex in all treated starfish were significantly slower than response times of controls (ANOVA, $F=9.53$, $d.f.=3,615$, $P<.001$; $LSD=4.26$, $d.f.=615$, $P=.05$). Thus at sublethal exposures of just six hours to all treatments, starfish were affected in response to and possibly recognition of food presented as a homogenate. Starfish showed no response to the mechanical stimulation of plain sea water.

Table V. Starfish response time (sec) for posturing reflex for treated and untreated starfish at 15°C and 20°C.

	Treatment			
	C	O	D	OD
\bar{X} (sec)	13.5	20.5	22.2	24.2
S.E.	1.1	1.6	1.7	1.7
N	160	155	160	144

C - Control

O - Kuwait Crude Oil

D - Corexit 9527 Dispersant

OD - Oil and Dispersant

3. Oyster Drill (Urosalpinx cinerea)

a. Methods

Oyster drills were tested for behavioral recognition of scallop effluent using the plywood choice chamber described in a previous paper (Ordzie & Garofalo, 1980b, see also section III). This chamber is used to demonstrate the ability of the drills to choose between scallop effluent and plain sea water. All twenty drills from the 12.5% concentration of each treatment and a control were tested in the apparatus. Animals from the four different treatments were tested in a random order each day.

Three U. cinerea, marked with nail polish for identification, were started in the center of the apparatus with their long axis perpendicular to the long axis of the chamber. Each drill was allowed an hour to respond. Distance moved in cm was recorded after an hour. If a drill reached the end of the ramp in less than one hour, distance and time in minutes were recorded. The distance moved was designated positive if drills moved toward the scallop effluent, and negative if they moved toward plain sea water. Daily testing was done four times during the depuration period and this experiment was replicated twice at 20°C (7/23/79) and 7/30/79). Distances traveled by drills from each treatment were analyzed with a one-way analysis of variance test. Rates (cm/min) traveled toward both scallop effluent and plain sea water were determined for each animal tested. A one-way analysis of variance test was used to determine treatment effect on rate of travel.

Previously we (Ordzie & Garofalo, 1980b, see also section III) performed blank tests in which untreated drills were tested for any left-right bias in the choice chamber. To do this, we presented plain sea water on both sides. Results showed no detectable bias at the behavioral level studied and it was then concluded unlikely that the apparatus would interfere with the observed results.

b. Results

Because there was no significant difference between replicates, results of both were combined. The net positive distance moved by treated drills was not significantly different (ANOVA) from distances moved by controls (Table VI). Compared to the net distance moved in blank tests, treated and control drills exhibit a large net positive movement toward scallop effluent. Similarly, there was no significant difference between treated and control drills for rates of travel toward scallop effluent (ANOVA).

Table VI. Distance traveled (cm) by treated and untreated drills toward scallop effluent in a choice chamber at 20°C.

	Treatment			
	C	O	D	OD
\bar{X} (cm)	5.1	5.0	5.1	4.6
S.E.	.9	1.0	1.0	.9
N	145	149	151	146

C - Control

O - Kuwait Crude Oil

D - Corexit 9527 Dispersant

OD - Oil and Dispersant

9.1.5 Discussion

The goal of this study was to examine effects of oil and dispersant on a predator-prey system during selected ambient water temperatures. It was not the purpose here to evaluate the relative toxic dangers of either substance to natural populations, but rather, to study how this predator-prey system responds, and to examine the merits of using such an ecological system in bioassay work.

At high concentrations of treatment solutions, each member of the scallop predator-prey system was affected differently. Scallop survivorship was decreased by any treatment solution which contained dispersant. Starfish were less affected, but when they were, they were susceptible only to the dispersant treatment while survivorship of the oyster drill was unaffected by any treatment. This differential susceptibility to high concentrations of solutions prepared in identical ways points to a problem biologists face when dealing with bioassay. Because not all animals are affected by the same chemicals at the same concentration and that animals have ecological relationships which should also be considered, knowing the response of one species to a number of pollutants is not always sufficient for ecological assessment.

The sequence for susceptibility at sublethal levels is somewhat different for each species tested. Scallops suffered decreased predator recognition when exposed to any treatment with dispersant, starfish were hindered in their recognition of scallops as food when exposed to any treatment, while drills showed no measureable effect of any treatment on their ability to detect and move toward scallops. Ultimately, in a

disrupted system, scallop populations may suffer more than the direct impact of a pollutant which selectively affects scallops but not all of the scallop predators.

This is a partial picture of what to expect from differential susceptibilities in a predator-prey system because information on long term consequences is also needed. Eisler (1973) noticed lower predation rates for Iranian Crude Oil and dispersant treated bivalve prey, as well as fecundity in predatory drills which fed on contaminated prey. In the future, studies which consider animals in more complete ecological context will provide better information about the impact of oil pollutants.

In light of the differential susceptibility demonstrated in this simple three animal system, the concept of an indicator species is difficult to defend. It would seem that because each organism can have its own array of chemical compound and concentration response, that there is no logical reason to assume that one animal could possibly be used to accurately judge susceptibility arrays for other species.

One major reason drills survived dosing is that they withdrew into their shells upon exposure, effectively isolating themselves from the environment. Dicks (1976) has suggested that withdrawn snails may suffer higher mortality in areas with high mechanical energy due to surf action. However, in areas with no violent mechanical action where scallops are found (coastal ponds) the survival of drills could be much higher than on the exposed coast.

In order to accurately assess biological effects of a pollutant event, we need to know susceptibilities of animals for different seasons. Seasonal sensitivity can be quite dramatic. Dispersant concentrations which are not lethal to scallops during winter temperatures cause greater than 50% mortality at summer temperatures. Although temperature of ambient water could be a significant predictor of scallop susceptibility to dispersant exposure, one should not generalize to other organisms. This issue becomes more complex because either the "pollutant toxicity" or "animal sensitivity" can be affected by temperature (Rice et al., 1977). Accordingly, the temperature related susceptibility can be different for each organism, making broad generalizations dangerous.

9.2 Section II

Behavioral Recognition of Mollusc and Echinoderm Predators by the Bay Scallop, Argopecten irradians (Lamarck) at two temperatures

Abstract

In an investigation of predator stimulated responses, bay scallops Argopecten irradians (Lamarck) were least sensitive on the dorsal side of their shell periphery. Scallops discriminated predatory from non-predatory gastropod molluscs and echinoderms based on scallop response times and swimming claps. Predatory test species Urosalpinx cinerea (Say), Asterias forbesi (Desor), Eupleura caudata (Say), Thais lapillus (L.), and Busycon canaliculatum (L.) provoked stereotypic escape responses. Although temperature had little effect on predator recognition, scallops required more time to respond to predators at 12°C than at 20°C. Once initiated, escape responses appeared to be temperature independent. It would seem predator recognition contributes to an efficient time-energy budget.

9.2.1 Introduction

Predatory starfish have been shown to evoke dramatic, predictable, escape responses from a variety of marine invertebrates (Bullock, 1953; Feder, 1967; Mackie, 1970; Ansell, 1969) including scallops (Thomas & Gruffydd, 1971; Feder, 1972; Stephens, 1978). Several molluscs (Bullock, 1953) and the scallop Pecten maximus (Thomas & Gruffydd, 1971) have been shown to differentiate, by touch, predatory from non-predatory starfish. They demonstrated that, although not as effective as contact, crude extracts of starfish were sufficient stimuli for provoking escape responses from P. maximus. Work on starfish substances responsible for evoking escape responses has shown that they come from tube feet (Feder & Lasker, 1964) and that they are surface active agents identified as "saponin-like" (Mackie et al., 1968) or steroid glycosides (Mackie, 1970). Among the echinoderms examined by Yasumoto et al. (1966), saponins were only present in starfish and were found to vary seasonally.

Although reports of starfish evoked escape responses are common in the literature, reports of predatory molluscs which elicit escape behavior are less frequent (Ansell, 1969; Gore, 1966). In this paper, we quantify and examine bay scallop, Argopecten irradians (Broom, 1976) responses to predatory and non-predatory echinoderms and gastropod molluscs at two temperatures.

9.2.2 Materials and Methods

A. Test Species

Bay scallops, A. irradians, were dredged or collected by diving in Point Judith Pond, Rhode Island. Scallop shell height averaged 50.1 ± 4.4 mm (mean ± s.e.). Scallops were maintained in a laboratory with running, unfiltered sea water from Point Judith Pond where the salinity averaged 31.7 ± .4 ppt. Predatory snails, Busycon canaliculatum,

Eupleura caudata, Urosalpinx cinerea, non-predatory snails Littorina littorea (L.), Ilyanassa obsoleta (Say), and a predatory starfish Asterias forbesi were collected from Point Judith Pond. Another predatory snail, Thais lapillus and a non-predatory sea urchin Arbacia punctulata (Lamarck) were collected from an exposed intertidal jetty outside the pond. All test invertebrates were maintained either in unfiltered, running sea water at ambient (10⁰ - 20⁰C) temperature or in a 30 liter all glass aquarium, fitted with aeration and temperature control. Water was changed every three days in the aquarium.

B. Scallop Behavior

Stimulation was accomplished by allowing the foot of a restrained snail to contact the mantle margin of an unrestrained scallop. The snail was held stationary by pressing the shell apex into a flexible tube, attached to the end of a rigid tube, which was suspended by an adjustable cross bar over the observation tray. A snail so stabilized could be positioned at any desired location and still have full foot mobility for stimulation.

Two aspects of scallop behavioral responses were measured. Response time, defined as the time from initial stimulation to first valve adduction, was measured in seconds with a stopwatch. If no response occurred within one minute, the observation was terminated and the scallop credited with a 60 second response time. The number of swimming claps was measured by counting valve adductions during a response.

It was necessary to first determine relative sensitivity of different sites on the scallop mantle margin before further testing. A priori four peripheral areas; dorsal, ventral, anterior wing, and posterior wing were chosen to test sensitivity to stimulation with a predator, U. cinerea (Fig. 1). Scallops were kept in a 50 liter all glass aquarium, with aeration and temperature at 12⁰C for seven days prior to testing. Aquarium water was replaced daily with fresh sea water throughout the experiment.

Each of four, epoxy coated, plywood observation trays contained five separate compartments (each compartment measured 27.5 cm long x 10.5 cm wide x 5 cm deep) to isolate individual scallops and eliminate presumed chemical communication. All scallops were allowed at least two minutes after handling to acclimate in the observation trays at 12⁰C before stimulation.

Twenty scallops were stimulated first at one area of the mantle margin, then the same twenty scallops were stimulated at another site, until all four areas had been tested. This procedure was replicated six times. The sequence for testing the four areas was changed for each replicate. Water in observation trays was replaced after each trial.

Scallop responses to all test species were measured at ambient temperatures of 20⁰C (August 1978) and 12⁰C (October 1978). Test species were brought in contact with the scallop mantle margin at the anterior wing. All snails, except B. canaliculatum, were presented using the plastic tube and crossbar apparatus described above. B. canaliculatum, because of its bulk, was hand held during stimulation as were starfish and sea urchins. Stimulation began when either snail foot

or echinoderm tube feet touched the scallop.

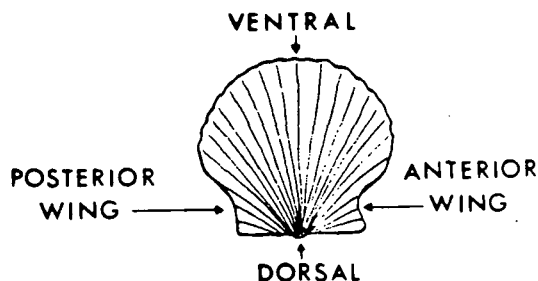


Fig. 1. Diagram of the bay scallop Argopecten irradians, with the four peripheral areas selected for stimulation as viewed from outside of left valve.

Twenty scallops were exposed to each test species. In all, eight different groups of twenty scallops were exposed to eight species. This was replicated three times. Presentation of test organisms was changed for each replicate so that no group of scallops was stimulated more than once by the same species. Both scallops and test species were maintained in running sea water at ambient temperatures. Sea water in observation trays was replaced after each test.

Data for both experiments, consisting of means of response times and swimming claps for groups of five scallops, were analyzed using the analysis of variance test (ANOVA). To examine effects of stimulation on four peripheral areas, a one-way ANOVA and the least significant difference (LSD) tests (Snedecor & Cochran, 1967; Sokal & Rohlf, 1969) were employed to identify differences among means. A two-way ANOVA and t-test were used to identify significant effects of test species and temperatures on scallop responses.

9.2.3 Results

A. Peripheral Sensitivity

Scallops showed varying sensitivity to stimulation with the predatory gastropod, U. cinerea, at selected sites on the mantle margin (Table I). Stimulation at either posterior or anterior wing resulted in significantly lower response times compared to results for dorsal or ventral sites and dorsal and ventral sites were different (ANOVA, $F = 137.7$, $df = 3$, 69 , $p = .01$; $LSD = 4.5$, $df = 92$, $p = .05$). While scallops stimulated at the dorsal site responded with significantly fewer swimming claps than for any other site, scallops stimulated at the anterior wing responded with the highest mean number of swimming claps (ANOVA, $F = 47.7$, $df = 3$, 69 , $p = .01$; $LSD = 1.1$, $df = 92$, $p = .05$). Based on these results, the anterior wing was selected as the site for all subsequent stimulation because scallops exhibited the most vigorous, least variable response at this location on the mantle periphery (Table I).

We observed predator proximity was not sufficient to consistently elicit escape behavior, therefore, all trials were performed with test organisms in physical contact with scallops.

Table I: Mean response time and mean number of swimming claps from scallops stimulated with *Urosalpinx cinerea* at four selected sites on the shell periphery.

	Peripheral Stimulation Sites			
	ventral	dorsal	posterior	anterior
Response Time				
\bar{X}	25.9	55.1	16.4	14.8
2 s.e.	4.6	3.2	4.2	3.2
Swimming Claps				
\bar{X}	5.6	0.8	5.6	7.1
2 s.e.	1.0	0.6	1.0	1.0

Table II: Mean scallop response times to eight test species at 12°C and 20°C. (* indicates predators)

Test species	Temperature	
	12°C	20°C
<u>Littorina littorea</u>		
\bar{X}	36.3	40.6
2 s.e.	7.4	4.8
<u>Arbacia punctulata</u>		
\bar{X}	55.6	56.5
2 s.e.	4.2	2.6
<u>Ilyanassa obsolata</u>		
\bar{X}	36.1	35.2
2 s.e.	8.2	5.4
<u>*Urosalpinx cinerea</u>		
\bar{X}	14.5	9.5
2 s.e.	4.8	3.0
<u>*Asterias forbesi</u>		
\bar{X}	12.5	8.5
2 s.e.	2.2	2.4
<u>*Eupleura caudata</u>		
\bar{X}	23.2	15.1
2 s.e.	4.6	3.4
<u>*Thais lapillus</u>		
\bar{X}	13.8	12.0
2 s.e.	4.2	3.2
<u>*Busycon canaliculatum</u>		
\bar{X}	24.5	20.0
2 s.e.	8.2	5.0

Table III: Mean number of scallop swimming claps in response to eight test species at 12°C and 20°C. (* indicates predators)

Test Species	Temperature	
	12°C	20°C
<u>Littorina littorea</u>		
\bar{X}	1.4	1.2
2 s.e.	0.6	0.6
<u>Arbacia punctulata</u>		
\bar{X}	0.2	0.3
2 s.e.	0.2	0.2
<u>Ilyanassa obsolata</u>		
\bar{X}	1.5	1.7
2 s.e.	0.6	0.6
<u>*Urosalpinx cinerea</u>		
\bar{X}	7.3	6.6
2 s.e.	1.0	1.0
<u>*Asterias forbesi</u>		
\bar{X}	4.3	3.8
2 s.e.	0.6	0.6
<u>*Eupleura caudata</u>		
\bar{X}	5.6	6.2
2 s.e.	1.4	0.8
<u>*Thais lapillus</u>		
\bar{X}	8.0	7.1
2 s.e.	1.4	1.2
<u>*Busycon canaliculatum</u>		
\bar{X}	6.5	5.1
2 s.e.	1.2	1.0

B. Response to Test Species

Quantified behavioral responses showed that scallops distinguished the predatory snails, U. cinerea, E. caudata, T. lapillus and B. canaliculatum and the predatory starfish A. forbesi, from the non-predatory snails, L. littorea and I. obsoleta and the non-predatory sea urchin, A. punctulata (Tables II and III).

There was a distinct difference among scallop responses to test species. When response time was plotted against number of claps (Fig. 2), two separate groups representing scallop responses to predators and non-predators became evident. Characteristically, scallops responded to predators quickly and vigorously as evidenced by lower mean response times and higher mean number of swimming claps. Further, scallops were able to carry out this discrimination and consistently distinguish predators from non-predators at both 12^o and 20^oC.

When responses to non-predators alone were examined, there was a significant effect on scallop behavior (Table IV). Mean response times were higher and mean number of swimming claps were lower when scallops were stimulated with A. punctulata compared to responses to either I. obsoleta or L. littorea (Fig. 2).

Responses to predators as a group were also significantly influenced by the test species used (Table IV) but were more varied (Fig. 2). Scallops responded to the starfish A. forbesi with fewer swimming claps than to any other test predator (t-test). However, response times to this starfish were similar to those for most predatory snails with the exception of higher response times to E. caudata (at 12^oC) and B. canaliculatum (t-test). Scallops exhibited the highest number of swimming claps when stimulated with T. lapillus and U. cinerea.

The significant temperature effect (Table IV) was evidenced by consistently lower mean response times to predators at 20^oC (Table II). No significant interactions between the effects of test species and temperature were observed.

9.2.4 Discussion

Sensitivity of four selected peripheral regions of the bay scallop, A. irradians, was variable and suggested that U. cinerea, at least, can successfully attack scallops from the dorsal hinge without evoking an escape response. In this region, the mantle is behind the hinge with no tentacles to contact an intruder. Responses to U. cinerea touching the dorsal hinge appeared to be due mainly to mechanical stimulation, evidenced by long response times and less than one swimming clap. Typical escape behavior which resulted from stimulation at three other areas, suggested scallops mechanically and chemically recognize U. cinerea primarily through tentacle contact with the snail rather than from chemical information in the water column. Others have found that physical contact with a predator provokes more reliable responses from various molluscs (Gore, 1966; Thomas & Gruffydd, 1971; Bullock, 1953; Turner, 1955).

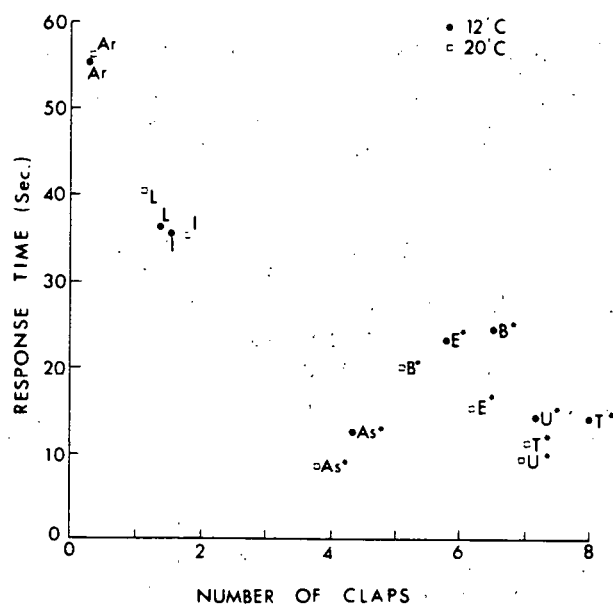


Fig. 2. Scattergram of mean scallop response time vs. mean number of swimming claps when stimulated with various test species at 12 and 20°C: Ar. *Arbacia punctulata*; L. *Littorina littorea*; I. *Ilyanassa obsoleta*; As*. *Asterias forbesi*; B*. *Busycon canaliculatum*; E*. *Eupleura caudata*; U*. *Urosalpinx cinerea*; T*, *Thais lapillus*; *, predators.

Table IV: A summary of F values and degrees of freedom (in parenthesis) for six analysis of variance tests. (* indicates $p < .05$)

	RESPONSE TIME		
	<u>All Data</u>	<u>Non-Predators</u>	<u>Predators</u>
Test Species (S)	*75.05 (7,165)	*26.31 (2,55)	*11.35 (4,99)
Temperature (T)	3.29 (1,165)	0.33 (1,55)	*12.31 (1,99)
Interaction (SxT)	1.08 (7,165)	0.37 (2,55)	0.55 (4,99)
	SWIMMING CLAPS		
	<u>All Data</u>	<u>Non-Predators</u>	<u>Predators</u>
Test Species (S)	*82.20 (7,165)	*13.71 (2,55)	*13.75 (4,99)
Temperature (T)	2.37 (1,165)	0.02 (1,55)	3.06 (1,99)
Interaction (SxT)	0.91 (7,165)	0.43 (2,55)	0.79 (4,99)

The feeding habits of the test species are quite varied. We observed U. cinerea, E. caudata and A. forbesi actively feeding on scallops during dives in Point Judith Pond. Although we did not observe B. canaliculatum, a known predator of scallops (Magalhaes, 1948), feeding, we captured a single individual near the scallop beds. Thais lapillus, however, is an unlikely predator of scallops because they are predominantly found in exposed, rocky intertidal habitats where they preferentially feed on barnacles (Connell, 1961). We never observed T. lapillus in or near the estuarine scallop beds in Point Judith Pond. Both non-predatory snails L. littorea, whose food preference is Ulva, Enteromorpha, and diatoms, (Newell, 1958) and I. obsoleta, which feeds mainly on microflora on the sediment on intertidal flats (Scheltema, 1964) were found on the scallop beds, while the sea urchin A. punctulata, which feeds primarily on Laminaria and Fucus (Lawrence, 1975) was not.

The ability of bay scallops to recognize predators through escape responses has been demonstrated here. While Thomas & Gruffydd (1971) have shown the scallop P. maximus capable of distinguishing predatory from non-predatory starfish, our results demonstrated bay scallops were capable of discriminating predatory from non-predatory gastropod molluscs. Further, bay scallops appeared equipped to recognize and escape from T. lapillus, even though this gastropod feeds in a different habitat. Appearance of escape responses then was generally correlated with feeding habits of the stimulating species and not with probability of encounter. Yarnall (1964) came to a similar conclusion for the escape response of Tegula funebris.

Although scallops discriminated a starfish from a sea urchin, responses to these echinoderms were less vigorous compared with scallop responses to gastropod molluscs. A partial explanation may be that echinoderms and gastropods provide scallops with very different chemical and mechanical stimuli for discrimination.

Ecologically, it is not surprising that bay scallops recognized predators at both 12°C and 20°C because scallop predators actively feed at these temperatures (Carriker & Van Zandt, 1972; Manzi, 1970; MacKenzie, 1969; Hanks, 1957). However, temperature did influence scallop response time to predators. Scallops took longer to respond at 12°C. At low temperatures, chemical sensitivity of the tentacles may decrease, or the amount of active substance from predators may be lower (Yasumoto, et al. 1966) or both. Whereas the number of swimming claps, caused by rhythmic activity in the adductor muscle and maintained by motor output from a stretch receptor feedback system (Stephens, 1978), seemed temperature independent, once initiated.

Predator discrimination, besides allowing prey to escape predators (Feder, 1963), could also reduce time and energy wasted on needless escape responses. Filter feeders are usually food limited and, as a consequence, their time-energy budget is such that they need to invest most of their time feeding (Wilson, 1975). Predator recognition could be used by scallops to minimize feeding interruptions. Thomas & Gruffydd (1971) have further reasoned that, since the scallop, P. maximus, often lives in depressions in the substrate, unnecessary escape responses could easily carry it out of a depression, forcing the scallop to invest extra time and energy in construction of a new depression. A similar case can be made for bay scallops which are often found in shallow depressions.

9.3 Section III.

Predation, attack success, and attraction to the Bay Scallop, Argopecten irradians by the Oyster Drill Urosalpinx cinerea

Abstract

Investigation of the intensity of predation by the oyster drill, Urosalpinx cinerea (Say), on the bay scallop, Argopecten irradians (Lamarck), was carried out in field and laboratory studies. Field measurements of densities of the oyster drill and the bay scallop were respectively, 3.6 m⁻², and 21.1 m⁻² on a scallop bed in Ninigret Pond, Charlestown, Rhode Island. The mean density of snails attacking scallops was 1.7 m⁻². In a laboratory study of attack success, an average of 72.3 percent of drill attacks led to death of the scallop. Snails were also shown to be strongly attracted to scallop effluent in a choice chamber.

9.3. Introduction

Barnacles, oysters, and mussels are often listed as primary prey for the oyster drill, Urosalpinx cinerea (Say) (Wood, 1968; Carriker & Van Zandt, 1972). It is also known that drills are guided by olfactory cues to their common prey (Wood, 1968; Pratt, 1974) but evidence that drills attack scallops is scarce although Marshall (1960) found that many U. cinerea were attracted to caged bay scallops in a Connecticut estuary. Our purpose was to determine the importance of U. cinerea as a predator of the bay scallop Argopecten irradians (Lamarck), on a natural scallop bed, to study drill attack success, and to examine the effect of scallop effluent on oyster drills in a choice chamber.

9.3.2 Methods & Results

9.3.3 Field Study

1. Methods

Field studies were carried out using SCUBA during July 1979 on a natural scallop bed in Ninigret Pond, Charlestown, Rhode Island. Square meter quadrats were randomly placed to measure scallop and oyster drill densities as well as the density of drill attacks. Attacks were defined as single or multiple occurrences of Urosalpinx cinerea attached to a live scallop. Densities were measured by removing all scallops and oyster drills from a m² quadrat after noting the number of drill attacks. Counts for each m² were made at the surface. Animals touching the square meter frame were considered to be within the quadrat. Mean densities were estimated from 21 m² quadrats. Temperature measurements ranged from 23^o - 26^oC while salinity was constant at 28 0/00. Scallops and drills collected during this phase were held in ambient running sea water for subsequent laboratory studies.

2. Results

The mean (+ 2 s.e.) scallop density on a scallop bed in Ninigret Pond was 21.2 ± 2.3 per m^2 , while the density of oyster drills was 3.6 ± 1.2 per m^2 . No other major predators, including the starfish Asterias forbesi (Desor), were observed during data collection. Although one blue crab, Callinectes sapidus (Rathbun), was found eating scallop remains, there was no evidence to show that the crab actually killed the scallop. The mean (+ 2 s.e.) density of attacks by Urosalpinx cinerea was 1.7 ± 0.6 per m^2 . Our calculations show that 7.9 percent of the scallops on this bed were being attacked by 47.0 percent of the drill population and that 6.8 percent of these scallops were attacked by more than one drill.

9.3.4 Laboratory Assessment of Oyster Drill Attack Success

1. Methods

To examine attack success, drills and scallops collected from Ninigret Pond, were placed in a tank (118 x 240 x 27 cm), with a bottom area of 2.8 m^2 . Only drills measuring 1.5 - 2 cm from apex to siphon were used. Prior to testing, all drills were provided with liberal numbers of live scallops on which to feed. After 24 hours, each scallop with a drill on its shell was isolated in a 40 liter tank with running sea water where the fate of each scallop could be monitored. Attacks were considered unsuccessful when a snail was found off of the scallop and successful if examination of a dead scallop revealed a completed borehole. Dead scallops with boreholes were assumed to have died directly or indirectly as a result of a snail attack. This procedure was replicated three times with different snails at a mean (± 2 s.e.) water temperature of $19.9 \pm .8^\circ C$ and a mean (± 2 s.e.) salinity of $30.0 \pm .4$ ‰ during August and September 1979.

2. Results

Of the attacking oyster drills, an average ($\bar{x} \pm 2$ s.e.) of 72.3 ± 9.8 percent succeeded with their attacks culminating in scallop death while only an average ($\bar{x} \pm 2$ s.e.) of 25.9 ± 12.2 percent of scallops survived attacks. Results of the three replicates are displayed in Table I. Although both replicates performed at $20^\circ C$ appear to be the same, attack success of snails at $17.7^\circ C$ tends to be lower even though it is not significantly different (chi-square). The mean time for success is similar at all temperatures, averaging 6.1 days (range: 2 - 15 days) with the majority of successful attacks occurring between day 4 and day 7.

9.3.5 Oyster Drill Response to Scallop Effluent

1. Methods

Scallop and oyster drills collected as previously described from Ninigret Pond were held in ambient temperature, unfiltered, running sea water for two weeks prior to experimentation. Oyster drills were supplied with live scallops for food. During the experiments, temperatures and salinities averaged ($\bar{X} \pm 2$ s.e.) $21.3 \pm 2.0^\circ C$ and $30.0 \pm .4$ ‰ respectively.

TABLE I

Laboratory assessment of the percentage of successful attacks by the oyster drill, Urosalpinx cinerea, on the bay scallop, Argopecten irradians, and mean time required to complete the attack.

	n	% successful attacks	% unsuccessful attacks	$\bar{X} \pm 2 \text{ s.e.}$ days until scallop death	$\bar{X} \pm 2 \text{ s.e.}$ temp. °C
Replicate 1 8/22 - 9/5	18	77.8	16.7	6.1 ± 1.5	20.9 ± 0.8
Replicate 2 8/29 - 9/4	17	76.5	23.5	5.9 ± 1.3	20.6 ± 0.8
Replicate 3 9/20 - 10/1	16	62.5	37.5	6.3 ± 2.1	17.7 ± 0.7
		$\bar{X} = 72.3$ 2.s.e. = 9.8	$\bar{X} = 25.9$ 2.s.e. = 12.2	$\bar{X} = 6.1 \pm 0.9$	$\bar{x} = 19.9 \pm 0.7$

Trials were carried out with epoxy coated plywood choice chambers designed by Pratt (1974). Continuously running sea water was first fed into two reservoirs (21 x 19 x 22 cm) from which the water was gravity fed into wells on both sides of the choice chamber. During tests, scallop effluent was introduced into sea water by placing thirty live scallops into one of the reservoirs. Water from the wells overflowed down both ramps a distance of 19.5 cm to exit through holes in a drain plate at the center of the apparatus. Flow rates to the wells were set with valves at 250 ml per minute. Dye experiments showed that mixing occurred only in a limited area over the drain plate holes. To eliminate possible directional bias, scallop effluent was presented on different sides of the choice chamber after six drills were tested.

Trials were performed by starting three marked snails directly in the center of the drain plate with their long axes perpendicular to the chamber length. After one hour, the distance in cm each drill traveled away from the start was measured from the center of the chamber to the tip of the drill siphon. Drills were replaced with new snails after they responded or if they failed to move from the starting position after an hour. Although Wood (1968) found that Urosalpinx cinerea do not follow each others trails, as a precautionary measure, ramps were scrubbed after every six drills tested with sea water during each trial. If a snail reached the well in less than an hour, both distance and time in minutes were recorded. During the first of two trials, 88 different drills were presented with plain sea water on both sides of the chamber to test for chamber bias. In the second trial, 100 different drills were presented with a choice between scallop effluent and plain sea water to measure drill response to scallops. Data were analyzed using the chi-square and t-test.

2. Results

When presented with a choice between plain sea water versus plain sea water in trial 1 (Table II), the number of Urosalpinx cinerea responding and moving greater than halfway up the ramp (10 cm) was the same for both sides of the chamber (chi-square). Measurements of the distance traveled and the rate that drills moved up either ramp showed no difference between sides, further indicating that there was no significant apparatus bias (t-test).

Responses of drills presented with a choice between sea water containing scallop effluent and plain sea water in trial 2 (Table II) showed a significant number of snails responded to scallop effluent compared to those responding to plain sea water (chi-square). The number of snails moving more than 10 cm was also greater in water containing scallop effluent (chi-square). Further, drills traveled twice the distance and speed in scallop effluent compared to distances traveled in plain sea water.

9.3.6 Discussion

Urosalpinx cinerea is an active predator of Argopecten irradians in Ninigret Pond, Rhode Island and was the only predator found during our observations. Although other predators have been listed as preying on scallops (Marshall, 1960) we have no data on their actual or potential

TABLE II

Responses of *Urosalpinx cinerea* to bay scallop effluent
and plain sea water in the choice chamber

Water Presented	Trial 1		Significance			
	Plain Sea Water	Plain Sea Water	χ^2	t-test	d.f.	P
	Trial 1 n = 88					
number responding	44	44	0.0	--	1	.99
number moving ≥ 10 cm	4	6	0.4	--	1	<0.1
$\bar{X} \pm 2$ s.e. cm traveled	2.6 \pm 1.4	3.8 \pm 1.8	--	1.04	86	>0.2
$\bar{X} \pm 2$ s.e. rate of movement (cm/min)	0.08 \pm 0.07	0.09 \pm 0.05	--	0.22	86	>0.5
	Trial 2 n = 100					
	Scallop Effluent	Plain Sea Water				
number responding	65	35	9.0	--	1	<0.005
number moving ≥ 10 cm	33	7	16.7	--	1	<0.005
$\bar{X} \pm 2$ s.e. cm traveled	10.8 \pm 2.0	5.4 \pm 2.2	--	3.36	98	<0.001
$\bar{X} \pm 2$ s.e. rate of movement (cm/min)	0.35 \pm 0.1	0.17 \pm 0.11	--	2.19	98	<0.05
	Trial 2 n = 100					
	Scallop Effluent	Plain Sea Water				
number responding	65	35	9.0	--	1	0.005
number moving 10 cm	33	7	16.7	--	1	0.005
$\bar{X} \pm 2$ s.e. cm traveled	10.8 \pm 2.0	5.4 \pm 2.2	--	3.36	98	0.001
$\bar{X} \pm 2$ s.e. rate of movement (cm/min)	0.35 \pm 0.1	0.17 \pm 0.11	--	2.19	98	0.05

impact in Ninigret Pond. During the spring, when water temperatures were 10°C, we observed Asterias forbesi preying on scallops in the study area. However, starfish were conspicuously absent from our summer observations, possibly owing to their inability to cope with temperatures above 25°C (Mackenzie, 1969). Further, our observations on laboratory held starfish confirm that mortalities were unusually high when ambient water temperature was above 20°C. U. cinerea, unlike starfish, feeds at a maximum rate (Hanks, 1957; Manzi, 1970) at the salinities and temperatures encountered during our observations.

Our laboratory studies show that not all drill attacks reach a successful conclusion. More than one quarter of all drill attacks on scallops are not successful and may be a direct result of the vigorous escape response (Ordzie and Garofalo, 1980) which bay scallops employ when attacked. Our observations indicate that the rapid movements of the scallop valves during this response were sufficient to shake off an attached drill. Further, we have observed live scallops in the field with complete and incomplete boreholes. Calculations of predation by U. cinerea on scallops based only on observed attacks without correction for unsuccessful attacks would lead to an overestimation of predation intensity.

Our measurements of time required to successfully drill scallops is an agreement with rates for U. cinerea to drill oysters, (Carriker and Van Zandt, 1972) and are similar to those found for Ocenebra japonica (Chew, 1960).

Environmental parameters have such strong influences on feeding rates of predatory snails (Menge, 1978) that predation rates differ between habitats and even between individuals. Such observations make it difficult to generalize about predation rates. The impact of predation is very specific for habitat location and environmental conditions.

We have also shown that U. cinerea move toward water containing scallop effluent. This strong attraction was heretofore only observed when drills were presented with barnacle effluent and is unusually strong compared to other bivalve species tested, including oysters (Wood, 1968; Pratt, 1974). Further, once stimulated, oyster drills proceed to double their rate of locomotion toward the scallops. Moving faster toward prey effluent increases the probability of prey encounter in a shorter time period. By decreasing the time between recognition of prey effluent and contact with mobile prey, drills also increase the probability of being able to execute an attack before the prey changed location.

9.4.1 Introduction

Investigations of community type responses were stimulated by results from previous work (Section 9.1) which suggested that sublethal concentrations of dispersants had adverse effects on scallop behavioral escape responses and starfish posturing reflex. These results led us to create a simple community and ask what would happen if both predator and prey were dosed and placed together in large laboratory tanks. How many scallops would survive in each treatment? Can we detect changes in individual spacing with treatment? The purpose here was to study a scallop-starfish community interaction after dosing under laboratory conditions.

9.4.2 Methods and Materials

Preparation of dosing stock solutions was identical to the method already described (Section 9.1). Stock solutions of each treatment, oil, dispersant, and oil-dispersant were diluted to make dosing mixtures of 12.5% stock solution and 87.5% sea water. This concentration was previously determined to be sublethal at 10°C for scallops (Section 9.1). Forty scallops and six starfish were statically dosed together in 20 liters of treatment solution for six hours with aeration. After dosing, all animals from each treatment, plus a control with starfish and a control without starfish were removed and randomly placed into respective 2.8m² epoxy coated plywood tanks filled to a height of 18 cm. A constant flow of ambient temperature sea water (20 liters/min) was provided to each of the five tanks representing each treatment. This experiment was replicated twice with temperatures and salinities averaging ($\bar{X} \pm 2$ s.e.) 12.1 \pm 1.2°C and 30.5 \pm .40/00 respectively during the experiments.

Scallops in the 2.8 m² tanks were at a density of 15 per m², well within the natural densities we found on a scallop bed (section 9.3). Since no data was available for starfish densities, we chose to use six.

After dosing, the number of living scallops in each tank was recorded for 15 days. Survivorship results were analyzed using the chi-square statistical test. Additionally, nearest neighbor distance (cm) of scallops was recorded for each treatment tank during the 15 days. The analysis of variance test was used to analyze the nearest neighbor data. Dead scallops were not removed until the end of the experiment to approximate field conditions.

9.4.3 Results

A. Survivorship

Data from both replicates was combined since no significant replicate difference was found. Scallop survivorship at day five for the community experiment was compared to a five day survivorship experiment previously completed (Section 9.1) at 10°C for scallops exposed to 12.5% stock solution without starfish (Table 1). 10°C was chosen since the average temperature for the community experiment was 13.1°C. Each treatment, oil, dispersant and oil-dispersant, was independently compared to the control for the experiment. There was no significant difference

TABLE 1 Scallop Survivorship (Percent Surviving) for the 12.5% Concentration of the Four Experimental Treatments; Without Starfish at Day Five and with Starfish at Day Five.
C - Control, O - Kuwait Crude Oil, D - Corexit 9527 Dispersant, OD - Oil and Dispersant, *, $P < 0.05$

Five Day Survivorship without starfish n = 80		Significance			Five Day Survivorship with starfish n = 80		Significance		
		x ²	d.f.	P			x ²	d.f.	P
Treatments									
C	100				93.8				
	99	.01	1	.95	87.6	.21	1	<.9	
O	87.5	.83	1	.5	65*	5.22	1	<.05	
OD	92.5	.29	1	.9	61.3*	5.82	1	<.01	

in survivorship between the control and the treatments when starfish were absent (100C) (X^2). However, with starfish present, survivorship in the dispersant and oil-dispersant treatments was significantly lower than for controls (X^2). At day 15 after dosing, with starfish present, scallop survivorship in the dispersant and oil-dispersant treatments was also significantly lower than controls (X^2) (Table 2).

There were no starfish mortalities in any treatment during the entire community experiment.

TABLE 2 Scallop Survivorship at (Percent Surviving) at 15 Days for the 12.5% concentration of the Four Experimental Treatments with Starfish. C - Control, O - Oil, D - Dispersant, OD - Oil-Dispersant, *, Significantly Different from control

		Percent Surviving with Starfish	x ²	Significance d.f.	P
TREATMENT	C	90			
	O	74.1	1.54	1	<.5
	D	48.8	12.22*	1	<.001
	OD	53.8	9.12*	1	<.01

9.44 Spacing

Scallop spacing was found to be significantly different in the oil-dispersant treated scallops (ANNOVA Table 3). The mean distance to nearest neighbor in the oil-dispersant tank was significantly higher than both the control without starfish and the control with starfish (ANOVA, $F = 7.11$, d.f. = 4, 50, $P = .0001$; LST = 6.75, d.f. = 50, $P = .05$). Nearest neighbor distance for the oil treated and the dispersant treated scallops was not different from the controls.

TABLE 3 Spacing of scallops in \bar{X} cm to Nearest Neighbor for Five Experimental Treatments: C - control without starfish, C starfish - Control with starfish, O - oil, D - Dispersant, OD - Oil and Dispersant. *P .05 <.05 ANOVA

	C	C Starfish	O	D	OD
\bar{X} cm	12.7	10.2	10.4	16.1	25.5*
2 S.E.	.95	1.64	1.44	3.62	9.7

9.4.5 Discussion

The goal of this study was to determine how a simple predator-prey community would be affected by oil, dispersant and an oil-dispersant treatment. Scallops and starfish had previously been tested separately with these same treatments and the behavioral changes (Section 9.1) suggested a community type experiment.

In our previous study, scallops were found to have diminished discrimination between predators and non-predators when treated with dispersant and oil-dispersant, but that oil treated animals were not significantly different from the control animals. Response to food by starfish was significantly slowed by all treatments. When both predator and prey were treated as a community, scallop survivorship was significantly reduced in the dispersant and oil-dispersant treatments beyond that expected because of hydrocarbon treatment or starfish predation alone. Since scallop survivorship in the oil treatment was not different from controls, the slowed ability of the starfish to respond to food did not appear to affect their ability to feed on scallops. This again shows the differential susceptibility of the test animals to pollutants (section 9.1).

Scallops were significantly farther apart in the oil-dispersant treatment. Perhaps it is a behavioral advantage at this time of year for scallops not affected by treatment to be closer together during spawning (personal communication, John Karlsson).

The two measured aspects of this experiment, survivorship and spacing, appeared to be affected, but not always by the same treatments. Only additional studies could begin to unravel the details of the various community responses reported. One overriding observation remains: at concentrations far below the LD 50, dispersant treated scallops suffer greater than 50 percent mortality in the presence of starfish. These results are not predicted by classical bioassay methods. Community studies are rare to non-existent in bioassay work but could prove extremely useful in the prediction of ecological impacts by dispersants.

ADDENDUM

Analysis of Hydrocarbons in Stock Solutions

Oil (Kuwait Crude)

Aromatic
26.34 mg/liter
Aliphatic
18.28 mg/liter
Total Hydrocarbons
44.62 mg/liter

Dispersant

Aromatic
19.54 mg/liter
Aliphatic
13.88 mg/liter
Total Hydrocarbons
33.42 mg/liter

Oil & Dispersant

Aromatic
39.14 mg/liter
Aliphatic
20.78 mg/liter
Total Hydrocarbons
59.92 mg/liter

Oil in mixture by difference

Aromatic
19.6 mg/liter
Aliphatic
6.9 mg/liter
Total Hydrocarbons
26.5 mg/liter

Seawater Control

Aromatic
0.46 mg/liter
Aliphatic
0.024 mg/liter

Total Hydrocarbons
.484 mg/liter

10.0 References

10.1 Section 2 References

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- 11.2.1 Bibliography I: Fisheries and Biological References
- 11.2.2 Bibliography II: Behavior and Effects of Hydrocarbons
- 11.2.3 Bibliography III: Mathematics and Descriptions of Physical Phenomena

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12.0 Appendices

12.1 Section 2 Appendices

12.1.1 Appendix A Error Analysis

12.1.2 Appendix B Measurement of Interfacial Tension

12.1.3 Power Input

Section 2. Appendix A - Error Analysis

The error in the measurement or calculation that appears in any quantity in an investigation is the net result of different errors in the measurements or calculations preceding it. Thus the average drop-size, hold-up and interfacial area carries errors in them that depend on the experimental technique involved in measuring them or the use of quantities that have errors in calculating them.

The drop-size was measured using a microscope, and the size could be measured up to 0.25 microns. Thus the maximum possible error that could have arisen in the measurement of drop-size was ± 0.25 microns.

The hold-up was measured using an Infra-red Spectrometer and within the range of measurement, the maximum error possible was ± 1 ppm.

Thus due to an error in the measurement of drop-size the Sauter mean was in error as follows.

$$\epsilon_{SM} = \frac{\sum n_j (d_j + \epsilon_j)^3}{\sum n_j (d_j + \epsilon_j)^2} = 0 (\epsilon_j)$$

Interfacial area was given by

$$A = \frac{6 \times \phi}{SM}$$

Due to an error in the measurement of hold-up and Sauter mean, the interfacial area could have an error up to

$$\frac{6(\phi + \epsilon_\phi)}{(SM + \epsilon_{SM})} = 0 (0.4 \text{ m}^2/\text{m}^3)$$

The experiments at room temperature varied over a range of about 2.5 C. The variation in viscosity over such a small range of temperature is less than 5 percent (45). The interfacial tension over the same range of temperature is estimated to vary by about 1 dyne/cm. The effect of temperature on the drop-size can be estimated by the correlation of Shinnar (32). The error in the average drop-size due to temperature is found to be

$$\text{constant} \times (\sigma + \epsilon_\sigma)^{5/8} = 0 (0.25 \text{ microns})$$

From the above discussion, it can be seen that the maximum error that could be expected in the measurement of the drop-size is of the order of ± 0.5 microns. The hold-up is estimated to be accurate to within ± 1 ppm and the interfacial area accurate to within $0.4 \text{ m}^2/\text{m}^3$.

Section 2. Appendix B - Measurement of Interfacial Tension

Interfacial tension of Kuwait crude oil-sea water system was investigated in the presence of a dispersant. The interfacial tension is an important parameter when studying the stability of liquid-liquid systems. A lower value of interfacial tension means that the energy necessary to break up the dispersed phase will be proportionally lower and the dispersion will be stable.

Molecules in the bulk liquid phase experience the same average force in all directions. But at the interface this is not the case. Since the molecules across the interface are of a different species the forces are not evenly balanced. This results in a condition in which the interface is in a state of tension. The name "Surface Tension" is used when the interface is between a liquid and a vapor, and "Interfacial Tension" when the interface is between two liquids or a liquid and a solid.

When it is desired to separate two liquid phases after they have been brought into intimate contact (e.g., in liquid-liquid extraction) the interfacial tension should be high so that the coalescence is rapid. On the other hand, when one liquid is to be dispersed in another liquid, the interfacial tension should be low so that the break up is rapid and the dispersion is stable.

With few exceptions, a third component tends to reduce the interfacial tension between two pure components. The reducing effect is more pronounced if the third component is more concentrated at the interface than in the bulk. This is the case when surfactants and dispersants are used. The interfacial tensions between two liquids is highest when pure, and falls off to zero at plait point.

When a liquid surface (or liquid-liquid interface) is newly formed, a finite time is needed for establishing the state of equilibrium. During this period surface tension (or interfacial tension) is time dependent. In the case of the formation of pure liquid interfaces, it has not yet been possible to measure tension before the final value has been achieved, because the time involved is very small. However, when dealing with solutions the time factors involved are quite large and it is possible to measure the interfacial tension in the transient state. Surface tension or interfacial tension before equilibrium has been established is called "dynamic" to distinguish it from the equilibrium or "static" value.

Methods of Measurement

1) Capillary height-method. This is probably the simplest method available. When a capillary is inserted below the interface of a two liquid system, due to the excess free energy of the interface, the liquid in the lower layer rises to a higher level within the capillary.

But for the crude oil water system under study, this method could not be used as the darker upper layer of the crude prevents observation of the capillary height which should be known to correlate the interfacial tension.

2) Drop Weight Method. In this method drops are allowed to form at the top of a capillary immersed in another liquid. From a knowledge of the dimensions of the drop and its weight it is possible to calculate the interfacial tension. Since drops have to be formed at a finite site this method is not applicable in systems where a surfactant is present.

3) Ring Method. A platinum ring is pulled up from the interface of the liquids whose interfacial tension is to be measured. The force that is necessary is measured by a torsion balance. Again this method is inapplicable as this is a dynamic method, for the reasons given above.

4) Bubble Pressure Method. The pressure difference across a bubble or drop in another liquid is proportional to the interfacial tensions. Therefore, if it is possible to measure the pressure difference across the bubble we should be able to calculate the interfacial tension. Being a dynamic method this had to be discarded in favor of a semi-static method.

5) Pendant Drop Method. Pendant drop method consists of making a drop form at the tip of a capillary tube and let it hang in the second fluid. If the density difference is not appropriate, the drop can be made to rise up from the tip of the capillary rather than let it hang. The shape of the drop reflects a balance between interfacial tension and the gravitational forces and can be used to measure the interfacial tension. The static nature of the method makes it suitable for use where diffusional effects are involved.

The shape of the pendant drop is determined by the fact that the change in the hydrostatic pressure in the vertical direction is balanced by an equivalent change in the Laplace pressure

$$\Delta P_Q = \frac{2\gamma}{b}$$

where b is the radius of curvature at the apex of the drop.

At point P, a distance z below the apex, the pressure drop is given

$$\begin{aligned}\Delta P_p &= \gamma \frac{1}{R_1} + \frac{1}{R_2} \\ &= \frac{2\gamma}{b} + (\rho_1 - \rho_2) gz\end{aligned}$$

where R_1 and R_2 are the radii of curvature. The above equation is rearranged into the following dimensionless form:

$$\frac{1}{R_1/b} + \frac{\sin \theta}{x/b} = 2 + \frac{\Delta \rho g b^2}{\gamma} \left(\frac{z}{b}\right) = 2 + \frac{z}{b} \beta$$

where $\beta = \frac{\Delta \rho g b^2}{\gamma}$

and $R_1 = \left[1 + \frac{dz}{dx} \right]^2 \frac{d^2z}{dx^2}$

Bashforth and Adams carried out the numerical integration of the above equation for a number of values of B. As the radius b is difficult to determine experimentally, Bashforth and Adams presented a table of x_e/b as a function of B, where x_e is the equation radius. i.e.,

$$x_e b = f(\beta) \quad \text{so that}$$

$$\gamma = \Delta \rho g x_e^2 / \beta [f(\beta)]^2$$

For larger drops only, the radius of curvature in the plane of the paper need be considered. In this case, the equation for γ becomes

$$\gamma = \Delta \rho g h^2 / 2$$

and this represented a limiting case where h is the distance from the apex to the equatorial line of the drop.

Porter made use of the tables of Bashforth and Adams to show that the

differences in $h^2/2x_e^2$ and $a^2/2x_e^2$ is accurately represented by

$$h^2/2x_e^2 - a^2/2x_e^2 = 0.3047 (h^3/x_e^3) (1 - 4h^2/x_e^2)$$

where

$$a^2 = 2\gamma/\Delta\rho g$$

This permits the direct calculation of the surface tension from knowledge of h and x_e , both of which are accurately measurable quantities.

β can also be written as

$$\beta = \Delta\rho g d_e^2/H, \text{ where}$$

$$H_2 = \beta (d_e/b)^2$$

The Bashforth and Adams tables were re-worked by several authors into a form giving $1/H$ as a function of $S = d_s/d_e$.

It should not be thought that the ratio S is unique. Any other well-defined dimensions of the drop can be employed. Winkel has suggested that d_{\min}/d_e can be used, where d_{\min} is the smallest diameter which is observed above the d_e plane for a certain range of shapes (26). However, such a choice seems to be disadvantageous because the minimum diameter is often near the tip of the capillary and it may be affected by the irregularities in its shape. In order to alleviate this problem, Roc, Bacchetta and Wong defined a series of diameters as given by:

$$Z_n = (n/10) d_e$$

where $n = 8, \dots, 12$ and the characteristic shape factor is given by:

$$S_n = d_n/d_e$$

A series of tables giving $1/h$ as a function of S_n has been computed by the integration of the fundamental differential equation by a digital computer.

Apparatus and Measurement Method

The apparatus consists of a capillary tube of approximately 0.1 cm diameter as shown in Figure 1. The tube was bent into the shape of 'L' and connected to a small reservoir. The reservoir has an overflow port

MEASUREMENT OF INTERFACIAL TENSION

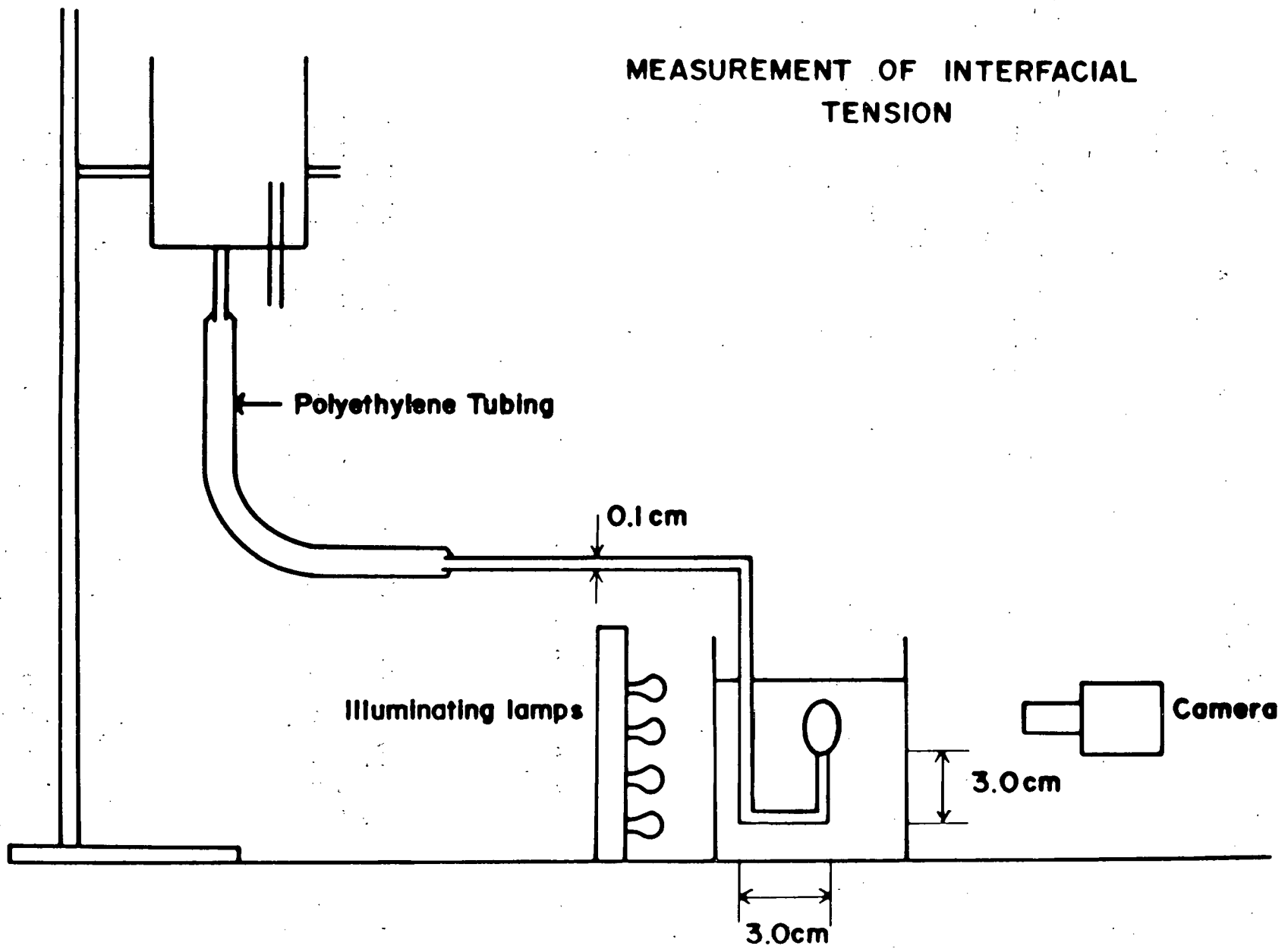


FIGURE 1.

and the crude oil is admitted to the reservoir in drops. The overflow port allows any excess crude to overflow thereby maintaining a constant head. The capillary tube is kept immersed in sea water.

Photographs were taken by a Mamiya Sekor camera provided with extension tubes for greater magnification. Magnification was indirectly determined by simultaneously photographing a steel ruler marked in 1/32" divisions.

Constant temperature could be maintained by a Haake EK11 refrigeration and cooling system of 200W capacity. A Versa Therm temperature probe and electronic relay (sensitivity 0.005 F) ensured that temperature was maintained under close control.

The tube and the reservoir were cleaned using a powerful laboratory cleaner "Micro," and then they were repeatedly rinsed in hot water to ensure that no traces of the cleaner remained on the capillary and the reservoir. The apparatus was then perfectly dried in an oven at 110 C. After each experiment, the apparatus was first washed using carbon tetrachloride and then the above procedure for cleaning was repeated.

A known volume of Corexit 9527 was added to the sea water (or to crude oil) and drops were allowed to form at the tip of the capillary at the rate of approximately one per minute. For each concentration level, 20 photographs were taken.

The photographs were projected on a screen and the largest diameter of each drop d_e was determined; d_s was measured at a distance of d_e from the vertex of the drop. The shape factor was determined and the corresponding value of $1/H$ was read from tables. Interfacial tensions were calculated using the formula:

$$\gamma = \frac{g \Delta \rho d_e^2}{H}$$

It is seen that, as shown, in Figure 2, the interfacial tension falls off rapidly as the concentration of the dispersant is increased. The decrease was most pronounced for the addition of the first 0.01% of the dispersant. Thereafter, the decrease in the interfacial tension is less rapid and it levels off at around 0.04% by volume of dispersant.

Results and Discussion

The interfacial tension data on the range 5°C to 22°C, as shown in Figures 2 and 4, shows the usual trends that would be expected with variations in temperature and concentration of the dispersant. The highest observed interfacial tension was 27.5×10^{-3} Newtons/Meter at 5 C and without dispersant, and the lowest was 2.75×10^{-3} Newtons/Meter at 22 C and 0.1 vol. % Corexit. Although 0.1 vol. % of Corexit is low when compared with usual dosages of surfactants, higher concentrations have not been used. At higher concentrations, the water becomes cloudy as the

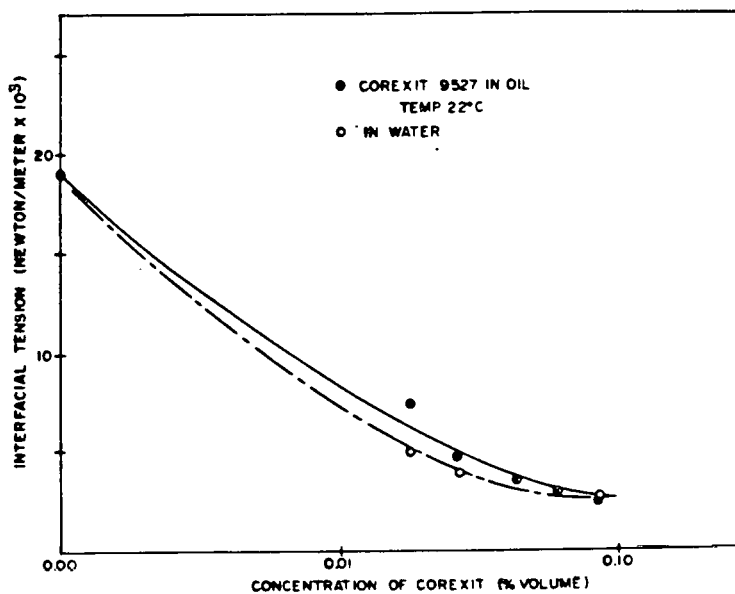


FIGURE 2.

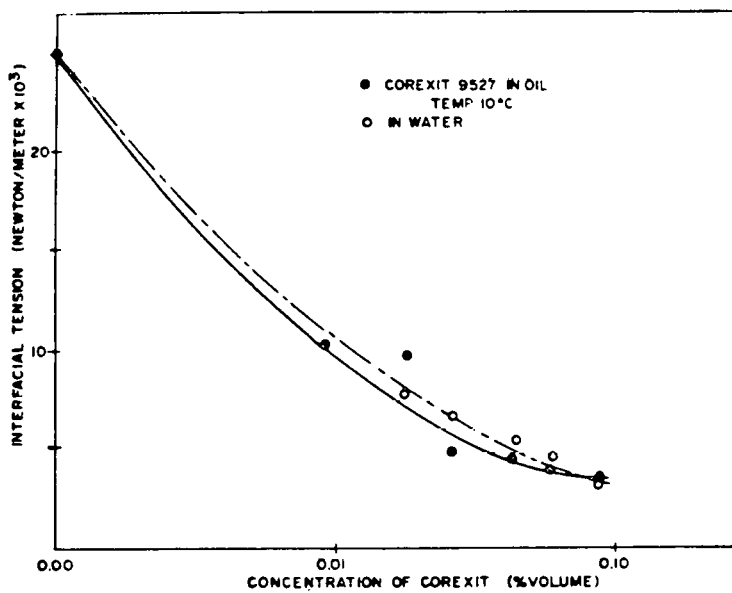


FIGURE 3.

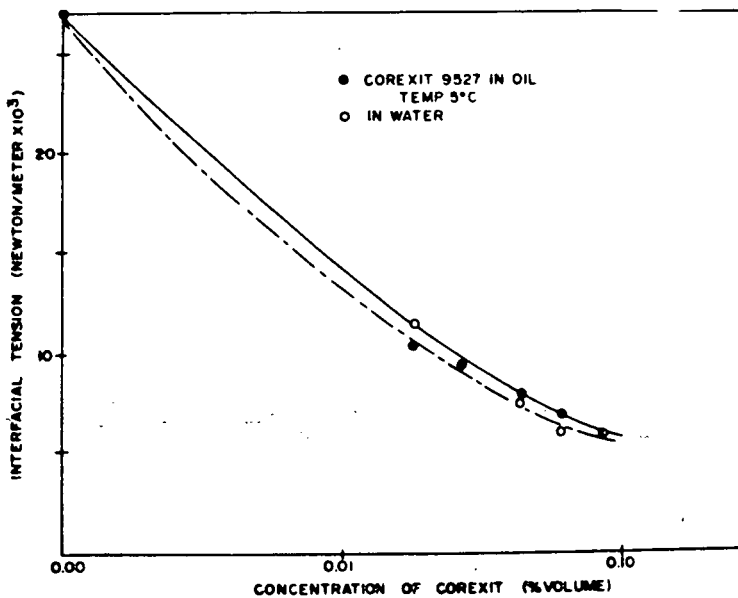


Figure 4.

concentration increases beyond the Critical Micelli Concentration and Tyndall effect becomes pronounced. Under these conditions, it is not possible to use the photographic method.

In analyzing the data, it was found that certain trends are unmistakable. It is seen that the largest drop in the interfacial tension is during the addition of the first 0 - 0.01 vol. % of Corexit. Thereafter the decrease is less with each incremental addition of Corexit and a plot of interfacial tension decreased by about 8.0×10^{-3} Newtons/Meter for the addition of the first 0.01 vol. % of Corexit. It should be possible to get lower values of interfacial tension by using a larger proportion of the dispersant. It has been observed in the past that concentrations as high as 1% (10 times the amount used in the present experiment) has been used.

Another fact which stands out is that it is immaterial in which phase the Corexit is added, as shown in Figures 2 and 4. Within limits of experimental error, it is seen that the interfacial tension observed are nearly equal. This is encouraging, as it is far easier to apply the dispersant on the oil, which is the top layer, than to apply it in water. Moreover, in the ocean, larger quantities of dispersant would be necessary, if the dispersant were to be applied on water.

The variation of interfacial tension with temperature, as shown in Figures 5 and 6, is what would normally be expected. There is a steady decrease in interfacial tension with increase in temperature. This is because the cohesion forces between the molecules falls off rapidly with increase in temperature and the interfacial tension is due to the attraction-force between the molecules at the interface. Unlike the variation of interfacial tension with concentration, which is rapid with the first increase in concentration, the decrease in interfacial tension with temperature is more or less uniform. On an average, the interfacial tension decreased by about 1×10^{-3} Newtons/Meter.

It was observed that at a given concentration level of Corexit and temperature, it did not matter to which phase Corexit was added. This could be because the intermolecular forces are reduced to the same degree in either phase at the same concentration level of Corexit and temperature (and interfacial tension is due to the net intermolecular forces at the interface). However, from a purely economical point of view, it might be advantageous to add Corexit to the oil phase, as in the ocean, because it takes a much larger quantity of Corexit in the aqueous phase to maintain the same concentration level.

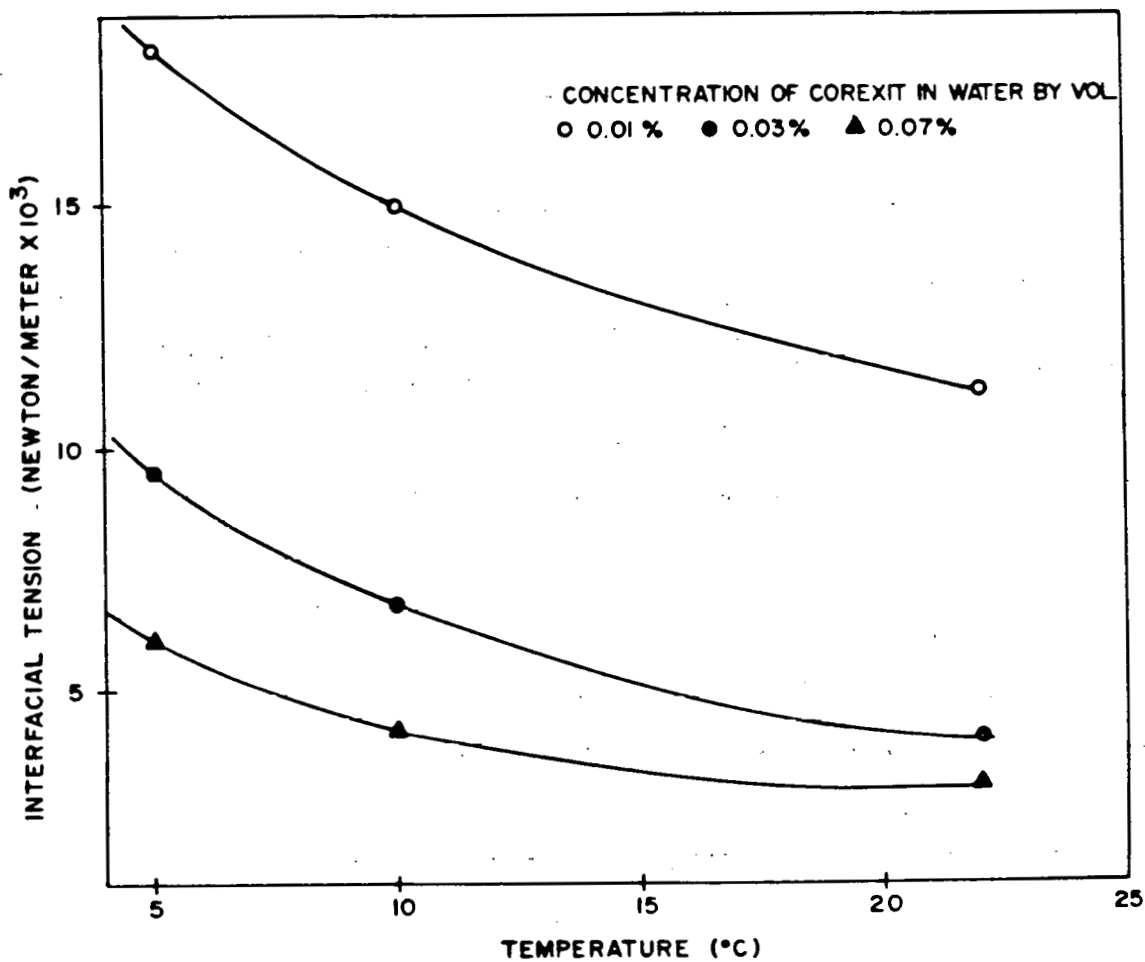


FIGURE 5.

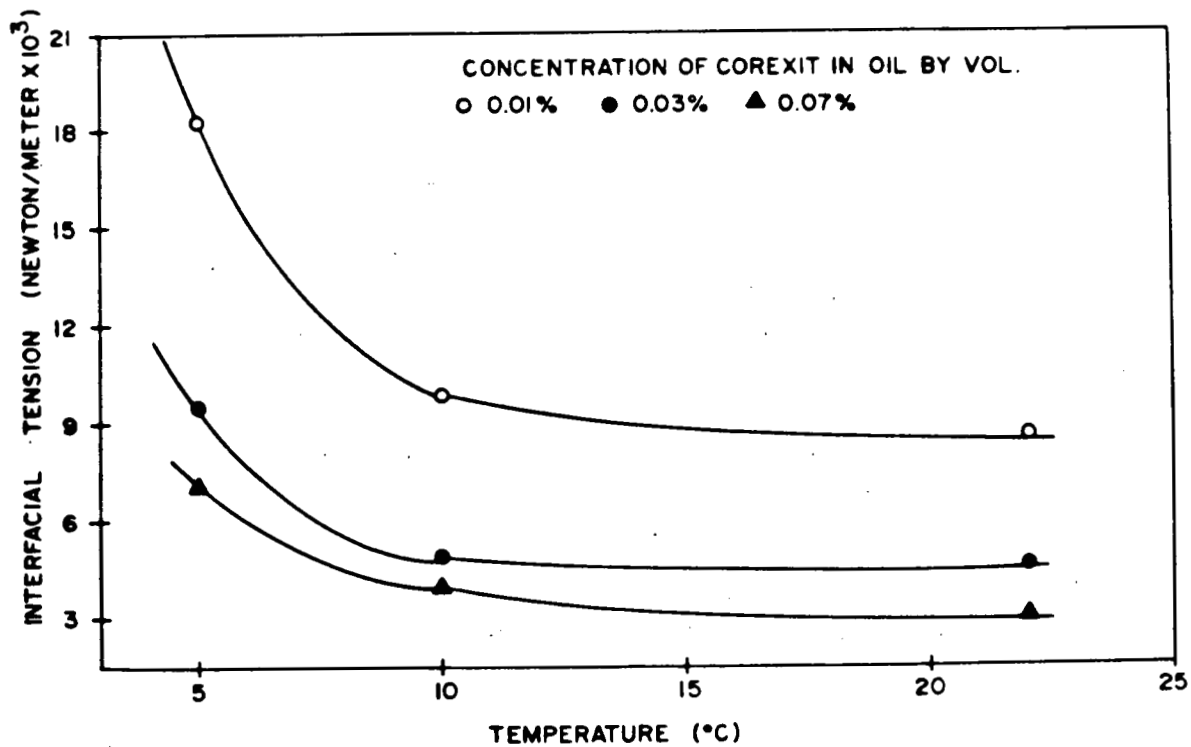


FIGURE 6.

INTERFACIAL TENSION

CONCENTRATION % VOLUME	COREXIT IN OIL			COREXIT IN WATER		
	50°C (x 10 ³ Newtons/Meter)	100°C (x 10 ³ Newtons/Meter)	220°C (x 10 ³ Newtons/Meter)	50°C (x 10 ³ Newtons/Meter)	100°C (x 10 ³ Newtons/Meter)	220°C (x 10 ³ Newtons/Meter)
0.00	27.10	25.10	19.10	27.10	25.10	19.10
0.01	18.40	10.50	8.75	18.40	15.00	11.20
0.02	11.59	9.80	7.50	11.47	8.00	5.10
0.03	9.51	5.00	4.90	9.54	6.80	4.10
0.05	8.14	4.72	3.74	7.60	4.54	3.73
0.07	7.15	4.11	3.11	6.16	4.18	3.15
0.10	6.16	3.91	2.74	6.01	3.73	2.75

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Section 2. Appendix C

Run No:	RPM	Rate of Power	Input (Joules)	Work Input for Inter- facial Area (Joules)	Percent Energy Utilized
1	150		52.31	33.90	4.32
2	150		52.31	161.82	9.24
10	300		99.30	52.05	6.63
14	300		99.30	196.79	25.08
9	100		11.30	43.13	5.50
13	100		11.30	156.46	19.93

12.2 Section 4.0 Appendices

- 12.1.1 Appendix A: Computer Program
- 12.1.2 Appendix B: Distinction Between Crude Oil and
Dispersant by Means of Infrared
Spectrophotometry
- 12.1.3 Appendix C: The Evaporation Tests

APPENDIX A

Computer Programs

Program name: STREAM

FNU(y^+) computes u^+ when y^+ is known from

$$y^+ = u^+ + A[\exp(\kappa u^+) - 1 - \kappa u^+]^2 / 2 - (\kappa u^+)^3 / 6 - (\kappa u^+)^4 / 24]$$

FNG(Re_x) computes ξ when Re_x is given from

$$Re_x = \int_0^{\xi} G(z) dz$$

FNF(ξ) computes $G(\xi)$

The program starts by asking for $Re_x (=X)$. It then computes

$$\left. \begin{array}{l} S = \xi \\ Y0 = y^+ \end{array} \right\} \text{which is printed}$$

It also computes the maximum permissible value for Re_y (based on the condition that $y^+ < y_0^+$) since the algebraic relations cease to be valid when $y^+ > y_0^+$.

For $Re_y = Y1$ to $Re_y = Y8$ in steps of $Y3$ will the program compute the following quantities:

$$U = u^+$$

$$Y5 = y^+$$

$$P = \psi^*$$

$$P1 = \psi^* + \xi B / \lambda$$

$$U5 = \bar{u} / U_0$$

$$V5 = \bar{v} / U_0$$

Program name: GSTREAM

The program operates at one specific value of y which is more or less determined by the input value ξ_0 . From this input the position Re_{x_0} and the value of $y_{0,0}^+$ are computed. The program then proceeds to compute \bar{u} / U_0 , \bar{v} / U_0 , v_{∞} / U_0 and $\tau / \rho U_0^2$ for increasing values of Re_x (defined through increasing values of ξ) whereby y is kept constant.

FNR(ξ) computes Re_x with ξ as input

Part 4.2: Eq.(2.10)
(See program: STREAM)

FNY(u^+) computes y^+ with u^+ as input

FNF(ξ) computes $G(\xi)$ with ξ as input Part 4.3: Eq.(2.5)

FNU(y^+) computes u^+ with y^+ as input (See program: STREAM)

PROGRAM NAME: STREAM

>>OLD:STREAM

>>LIST

```

00100      DEF FNF(T)
00110      A = 0.1108
00120      K = 0.4
00130      T1 = T*K
00150      G1 = 2+T1**3*(1/3+T1*(1/4+T1*(1/10+T1/36)))
00160      G = T**3/3+A*(EXP(T1)*(T1**2-2*T1+2)-G1)/(K*K)
00170      FNF = G
00180      FNEED
00360      DEF FNU(S)
00370      K = 0.4
00380      A = 0.1108
00390      Z = 30
00400      Z1 = Z*K
00410      S1 = Z+A*(EXP(Z1)-1-Z1-Z1**2/2-Z1**3/6-Z1**4/24)
00420      D2 = 1+A*K*(EXP(Z1)-1-Z1-Z1**2/2-Z1**3/6)
00430      D3 = S1-S
00440      D1 = ABS(D3)
00450      IF D1 < 0.001 THEN GO TO 490
00460      Z = Z-D1/D2
00470      PAUSE
00480      IF D1 > 0.001 THEN GO TO 400
00490      FNU = Z
00500      FNEED
00550      DEF FNG(S)
00560      K = 0.4
00570      A = 0.1108
00580      Z = 30
00590      N = 0
00600      Z1 = Z*K
00610      S4 = 6+2*Z1+Z1**4*(1/12+Z1*(1/20+Z1*(1/60+Z1/252)))
00620      S3 = EXP(Z1)*(Z1**2-4*Z1+6)-S4
00630      S1 = Z**4/12+A*S3/(K**3)
00640      D4 = 2+Z1**3*(1/3+Z1*(1/4+Z1*(1/10+Z1/36)))
00650      D3 = EXP(Z1)*(Z1**2-2*Z1+2)-D4
00660      D2 = Z**3/3+A*D3/(K**2)
00670      D3 = S1-S
00680      D1 = ABS(D3)
00690      IF D1 < 0.001 THEN GO TO 750
00700      Z = Z-D1/D2
00710      N = N+1
00720      IF N > 20 THEN GO TO 750
00730      PAUSE
00740      IF D1 > 0.001 THEN GO TO 600
00750      FNG = Z
00760      FNEED
00800      A = 0.1108
00810      K = 0.4
00820      PRINT 'PARTICLE SIZE P2=?'
00830      INPUT P2
00840      PRINT 'REX=?'

```

```
00850 INPUT X
00860 S = FNG(X)
00870 X1 = X*K
00880 S1 = S*K
00890 Y0 = S+A*(EXP(S1)-1-S1*(1+S1/2*(1+S1/3*(1+S1/4))))
00900 Y9 = Y0*S
00910 PRINT 'Y0='Y0,'KSI='S,'STOP VALUE Y9='Y9
00920 PRINT 'START VALUE Y1=?'
00930 INPUT Y1
00940 PRINT 'STEP Y3=?'
00950 INPUT Y3
00953 PRINT 'END VALUE Y8=?'
00955 INPUT Y8
00960 FOR Y = Y1 TO Y8 STEP Y3
00970 Y5 = Y/S
00980 U = FNU(Y5)
00990 U1 = U*K
01000 P3 = U1**2*(1/2+U1*(1/3+U1*(1/8+U1/30)))
01010 P = U**2/2+A*(EXP(U1))*(U1-1)-P3)
01020 P1 = P+P2*X
01021 U5 = U/S
01022 V5 = Y5*U/(S*FNF(S))
01030 PRINT Y,U5,V5,P,P1
01040 NEXT Y
01050 END
```

>>OLD:GSTREAM

>>LIST

4

```
00010 DEF FNR(L)
00020 A = 0.1108
00030 K = 0.4
00040 S1 = L*K
00050 R4 = 6+2*S1+S1**4*(1/12+S1*(1/20+S1*(1/60+S1/252)))
00060 R3 = EXP(S1)*(S1**2-4*S1+6)-R4
00070 R = L**4/12+A*R3/(K**3)
00080 FNR = R
00090 FNEND
00100 DEF FNY(J)
00110 A = 0.1108
00120 K = 0.4
00130 J1 = J*K
00140 Y = J+A*(EXP(J1)-1-J1*(1+J1*(1/2+J1*(1/6+J1/24))))
00150 FNY = Y
00160 FNEND
00170 DEF FNF(T)
00180 A = 0.1108
00190 K = 0.4
00200 T1 = T*K
00210 G1 = 2+T1**3*(1/3+T1*(1/4+T1*(1/10+T1/36)))
00220 G = T**3/3+A*(EXP(T1)*(T1**2-2*T1+2)-61)/(K*K)
00230 FNF = G
00240 FNEND
00250 DEF FNU(F)
00260 K = 0.4
00270 A = 0.1108
00280 Z = 30
00290 Z1 = Z*K
00300 F1 = Z+A*(EXP(Z1)-1-Z1-Z1**2/2-Z1**3/6-Z1**4/24)
00310 D2 = 1+A*K*(EXP(Z1)-1-Z1-Z1**2/2-Z1**3/6)
00320 D3 = F1-F
00330 D1 = ABS(D3)
00340 IF D1 < 0.001 THEN GO TO 380
00350 Z = Z-D1/D2
00360 PAUSE
00370 IF D1 > 0.001 THEN GO TO 290
00380 FNU = Z
00390 FNEND
00400 DEF FNG(H)
00410 K = 0.4
00420 A = 0.1108
00430 Z = 30
00440 N = 0
00450 Z1 = Z*K
00460 H4 = 6+2*Z1+Z1**4*(1/12+Z1*(1/20+Z1*(1/60+Z1/252)))
00470 H3 = EXP(Z1)*(Z1**2-4*Z1+6)-H4
00480 H1 = Z**4/12+A*H3/(K**3)
00490 D4 = 2+Z1**3*(1/3+Z1*(1/4+Z1*(1/10+Z1/36)))
00500 D3 = EXP(Z1)*(Z1**2-2*Z1+2)-D4
00510 D2 = Z**3/3+A*D3/(K**2)
00520 D3 = H1-H
00530 D1 = ABS(D3)
00540 IF D1 < 0.001 THEN GO TO 600
00550 Z = Z-D1/D2
00560 N = N+1
00570 IF N > 20 THEN GO TO 600
00580 PAUSE
00590 IF D1 > 0.001 THEN GO TO 450
00600 FNG = Z
00610 FNEND
```



```

00620  A = 0.1108
00630  K = 0.4
00640  PRINT 'KSINULL =?'
00650  INPUT S0
00660  S1 = S0*K
00670  Y0 = FNY(S0)
00675  R0 = FNR(S0)
00676  V0 = Y0*FNU(Y0)/(S0*FNF(S0))
00677  PRINT 'VNULL='V0
00680  PRINT 'KSINULL='S0, 'YNULL='Y0, 'REYNULL='R0
00690  PRINT 'END VALUE KSI=?'
00700  INPUT S9
00710  PRINT 'STEP KSI=?'
00720  INPUT S5
00730  FOR S = S0 TO S9 STEP S5
00740  Y = Y0*S0/S
00750  U = FNU(Y)/S
00751  P1 = U*S
00752  P2 = FNF(P1)/FNF(S)
00753  P = (1-P2)/(S*S)
00760  V1 = S*FNF(S)
00764  Y9 = FNY(S)
00765  V9 = Y9*FNU(Y9)/(V1*V0)
00770  V = Y*FNU(Y)/(V1*V0)
00775  R = FNR(S)-R0
00780  PRINT S,P,U,V,R
00790  NEXT S
00800  END

```

Print-out for Fig. 3

KSINULL =?

[>15

VNULL= .00703263

KSINULL= 15 YNULL= 46.957908

REYNULL= 12629.96

END VALUE KSI=?

[>20

STEP KSI=?

[>0.5

15	0	1	1	0	1
15.5	.00115406	.96158019	.7084875.	3838.0247	.9070911
16	.00186284	.92571157	.50312827	8878.9309	.82728601
16.5	.00227983	.89215284	.35824054	15497.236	.75837591
17	.00250648	.86069193	.25581189	24179.827	.69852602
17.5	.00260981	.83114171	.18322563	35558.227	.64622587
18	.00263406	.80333643	.13164788	50449.782	.60023773
18.5	.00260838	.77712878	.09489072	69910.219	.55954812
19	.002552	.7523874	.06861478	95300.586	.52333076
19.5	.00247752	.72899485	.04977179	128372.43	.49090863
20	.00239319	.70684572	.03621569	171376.17	.46172682

PRINT OUT FOR FIG. 4

KSINULL =?

[>18

VNULL= .00422125

KSINULL= 18 YNULL= 143.32901

REYNULL= 63079.742

END VALUE KSI=?

[>25

STEP KSI=?

[0.5

> 18

	-1.894839E-08	1.0000006	1	0	1
18.5	.00076668	.96918672	.72214019	19460.437	.93221088
19	.00125915	.94008651	.52315133	44850.804	.87187251
19.5	.00156637	.91256516	.38019468	77922.646	.81785701
20	.00174857	.88649923	.27716206	120926.39	.76923993
20.5	.0018466	.86177837	.20266502	176748.9	.72526075
21	.00188823	.83830301	.14862894	249088.18	.68529128
21.5	.00189237	.81598306	.10931142	342674.99	.64880993
22	.00187191	.79473688	.08061594	463553.37	.61538148
22.5	.00183567	.77449024	.05961064	619436.23	.58464061
23	.00178965	.75517554	.04419039	820155.5	.55627881
23.5	.00173792	.73673112	.03283879	1078230.4	.53003404
24	.00168326	.71910054	.02446001	1409587.4	.50568231
24.5	.00162752	.70223214	.01825965	1834467.4	.48303115
25	.00157196	.68607848	.01366004	2378572.5	.46191407

PRINT OUT FOR FIG. 5

KSINULL =?

[>26

VNULL= .00178863

KSINULL= 26 YNULL= 3584.8098

REYNULL= 4026709.8

END VALUE KSI=?

[>30

STEP KSI=?

[>0.5

26	0	1	1	0	1
26.5	.00033301	.9793503	.75331917	1134665.1	.95913873
27	.0005654	.9594982	.56849313	2581174.1	.9207629
27.5	.00072512	.94039904	.4297397	4423392.3	.88466672
28	.00083233	.92201132	.32537806	6767345.5	.8506668
28.5	.00090164	.90429662	.24674257	9746983.4	.81859909
29	.00094362	.88721917	.1873893	13531445.	.78831623
29.5	.00096596	.87074568	.14251616	18334167	.75968551
30	.00097423	.85484512	.10853686	24424341	.73258681

FNG(Re_x) computes ξ with Re_x as input Part 4.2: Eq.(2.10)

With S(=) as variable from S = S0 to S = S9 in steps of S5 the program computes.

$$\bar{u}/U_0 = U \quad \text{Part 4.2: Eq.(2.3)}$$

$$\bar{v}/U_0 = V \quad \text{Part 4.2: Eq.(2.9)}$$

$$Re_x - \bar{n}e_{x_0} = R \quad \text{Part 4.2: Eq.(2.10)}$$

$$\tau/\rho U_0^2 = P \quad \text{Part 4.2: Eq.(2.16)}$$

$$\bar{v}'/U_0 = V\theta \quad \text{Part 4.2: Eq.(2.9)}$$

Program name: OIL2

The program operates at one specific value of $X(=\xi)$ which it asks for as input to start the computations. It computes the velocity components \bar{U} and \bar{V} , the stream function Ψ and the path-function θ and runs a table for running argument y/A .

FNF(η) COMPUTES:

$$FNF(\eta) = f(\eta) = \exp(-\eta^2) - 2B\eta^2 / (\sqrt{\pi}(B^2 + \eta^2)^2) \quad \text{Part 4.2: Eq. (4.3)}$$

FNE(η) COMPUTES:

$$FNE(\eta) = \frac{1}{2} \sqrt{\pi} \operatorname{erf}(\eta)$$

With Z1 as the input variable from Z1 Z0 to Z1=Z9 in steps of Z3 the following quantities are computed:

$$y/A \quad Z1 = y/A \quad (\text{input variable})$$

$$\eta \quad \xi = \frac{y}{A} (1 + \xi^2)^{-\frac{1}{2}} \quad \text{Part 4.2: Eq.(4.2)}$$

$$\bar{u}/U_0 \quad U = f(\eta) (1 + \xi^2)^{-\frac{1}{4}} \quad \text{Part 4.2: Eq.(4.1)}$$

$$\int f(\eta) d\eta \quad V\theta = \frac{1}{2} \sqrt{\pi} \operatorname{erf}(\eta) + \left[\frac{\eta/B}{1 + (\eta/B)^2} - \operatorname{arc tan}(\eta/B) \right] / \sqrt{\pi} \quad \text{Part 4.2: Eq.(4.5)}$$

$$V1 = 2\eta f(\eta) - \int f(z) dz$$

$$\bar{v}/U_0 \quad V = \frac{1}{2} \xi [2\eta f(\eta) - \int f(z) dz] (1 + \xi^2)^{-\frac{3}{4}} \quad \text{Part 4.2: Eq.(4.1)}$$

$$\Psi^* \quad P = (1 + \xi^2)^{\frac{1}{4}} \int f(z) dz \quad \text{Part 4.2: Eq.(4.7)}$$

$$\theta \quad P1 = \Psi^* + \xi B/\lambda \quad \text{Part 4.3: Eq.(2.22)}$$

>>OLD:OIL2
>>LIST

```

00010 DEF FNF(A)
00015 B = 5
00020 C1 = EXP(-A**2)
00030 C2 = 2*B*A**2
00040 C3 = (B**2+A**2)**2
00050 C4 = ATN(1)*4
00060 C5 = C4**0.5
00070 FNF = C1-C2/(C5*C3)
00080 FNFEND
00090 DEF FNE(D)
00091 IF D > 3.0 GO TO 165
00100 B = 5
00101 N = 0
00105 D3 = D
00106 D2 = D
00110 D2 = -D2*D**2*(2*N+1)/((2*N+3)*(N+1))
00120 D3 = D3+D2
00130 D4 = D2/D3
00140 N = N+1
00150 D5 = ABS(D4)
00160 IF D5 > 0.00001 THEN GO TO 110
00161 IF D5 < 0.00001 THEN GO TO 170
00165 D3 = 0.88623
00170 FNE = D3
00180 FNFEND
00209 PRINT 'PARTICLE SIZE P2=?'
00210 INPUT P2
00211 PRINT 'Z0=?'
00212 INPUT Z0
00213 PRINT 'Z9=?'
00214 INPUT Z9
00215 PRINT 'Z3=?'
00216 INPUT Z3
00217 PRINT 'X=?'
00218 INPUT X
00220 FOR Z1 = Z0 TO Z9 STEP Z3
00225 N1 = 0.5
00230 Z = Z1/((X**2+1)**0.5*2*N1)
00240 U = FNF(Z)/((X**2+1)**0.25)
00250 V2 = (ATN(1)*4)**0.5
00260 V3 = Z/B
00270 V4 = V3/(1+V3**2)-ATN(V3)
00280 V5 = FNE(Z)+V4/V2
00290 V1 = 2*Z*FNF(Z)-V5
00292 P = V5*(1+X**2)**0.25
00293 U = V1*X*N1/((1+X**2)**0.75)
00294 P1 = P+P2*X
00300 PRINT Z1,U,V,P,P1
00310 NEXT Z1
00320 END

```

APPENDIX B

Distinction between Crude Oil and Dispersant
by Means of Infrared Spectrophotometry

by

Mathew Cherian, Ted Kawazoe and Leif N. Persen

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Distinction between Crude Oil and Dispersant by means of Infrared Spectrophotometry

by

Mathew Cherian, Ted Kawazoe and Leif N. Persen

In investigations involving the use of a dispersant to influence the fate of an oil spill at sea (or on lakes) samples are usually taken from the water column. The hydrocarbons in the samples are extracted by some standard method and the concentration of hydrocarbons can be determined. If gas chromatography is used it is comparatively easy to determine how much of the hydrocarbons in the sample originates from the crude oil and how much from the dispersant, even though the process may be somewhat time consuming and requires expensive equipment. Apart from the obvious interest such distinction between oil and dispersant has when judging the effect of the dispersant the possible difference in toxicity of the two compounds makes this distinction important.

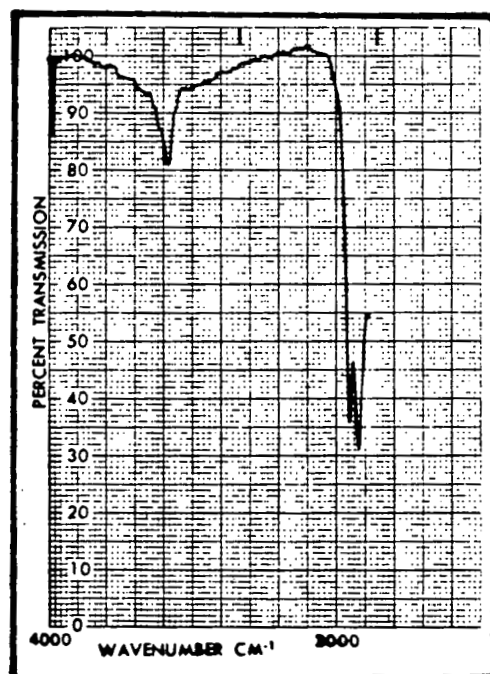


Fig. 1. The peaks at 3600 [cm^{-1}] and at 2930 [cm^{-1}] of Corexit 9527.

When a large number of samples are to be handled within a certain time limit a quick method which allows a distinction to be made between dispersant and crude oil recovered in the water samples is desirable. The following is a presentation of a method developed for infrared spectrophotometry.

The dispersant to be used is Corexit 9527 and the oil is standard Kuwait Crude. The extraction is supposed to utilize carbontetrachloride (CCl_4) and all samples in this investigation are prepared with this solvent. If Kuwait Crude is scanned in the infrared spectrophotometer one finds the usual peak at a wave number of $2930 [\text{cm}^{-1}]$. If however Corexit 9527 is scanned one finds an additional peak at a wave number of $3600 [\text{cm}^{-1}]$ as shown in Fig. 1. Most dispersants available commercially should give a peak at $3600 [\text{cm}^{-1}]$. This peak is due to the OH stretching, while the peak at 2930 is due to CH stretching. Since no peak is present for Kuwait Crude at the latter wave number, one has a possible basis for establishing the desired method.

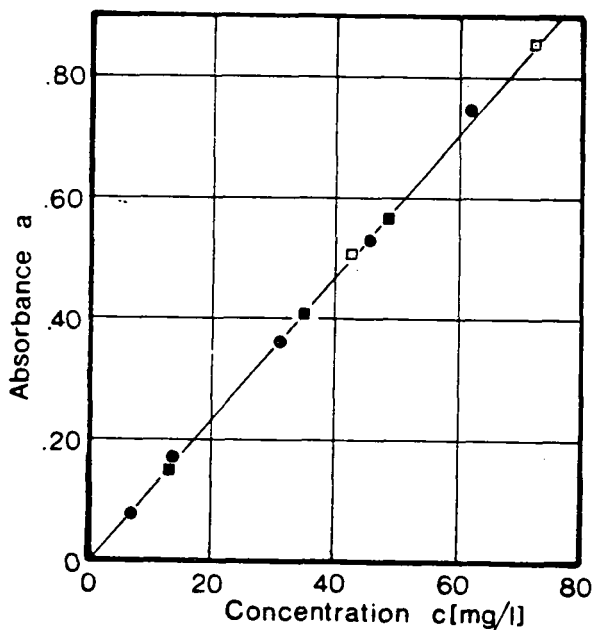


Fig. 2. Calibration curve for Kuwait Crude scanned at $2930 [\text{cm}^{-1}]$

First, the calibration curve for Kuwait Crude is established as shown in Fig. 2. Samples with different concentrations c_o of oil in CCl_4 are prepared and scanned at a wave number of $2930 [\text{cm}^{-1}]$. From the transmittance z thus obtained the absorbance a is computed

$$a = \log_{10}(100/z) \quad (1)$$

The results are shown in Fig. 2 which indicate a linear relationship between a and c . A linear regression based on the data obtained gives

$$a = 0.01179 c_0 - 0.00299 \pm 0.00316 \quad (2)$$

This is a standard result and the only comment one might add is that the accuracy is satisfying for concentrations down to 3-5 [mg "oil"/l CCl_4]

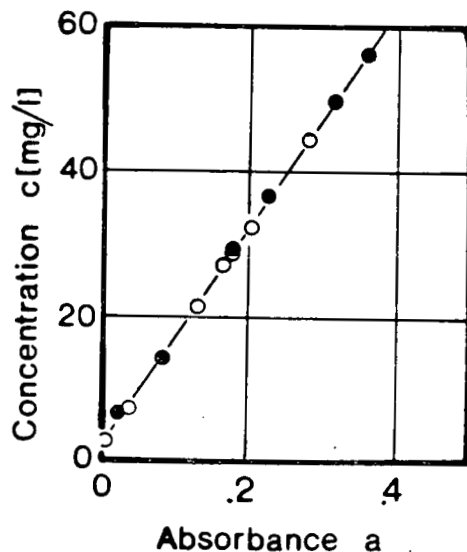


Fig. 3. Calibration curve for Corexit 9527 scanned at 2930 [cm^{-1}].

The next step is to prepare samples with Corexit 9527 in different concentrations c_c in CCl_4 . Scanning these at a wave number of 2930 [cm^{-1}] and computing the absorbance one obtained the results shown in Fig. 3. Again a linear relationship between the concentration and the absorbance is evident and a linear regression applied to the data gives

$$a = 0.00665 c_c - 0.01516 \pm 0.00314 \quad (3)$$

Again this is a result which could be expected, the only obvious remark being that the sensitivity to concentrations of Corexit 9527 is lower than to Kuwait Crude.

If samples with Corexit alone is scanned at a wave number of 3600 [cm^{-1}] a calibration curve as shown in Fig. 4A is found:

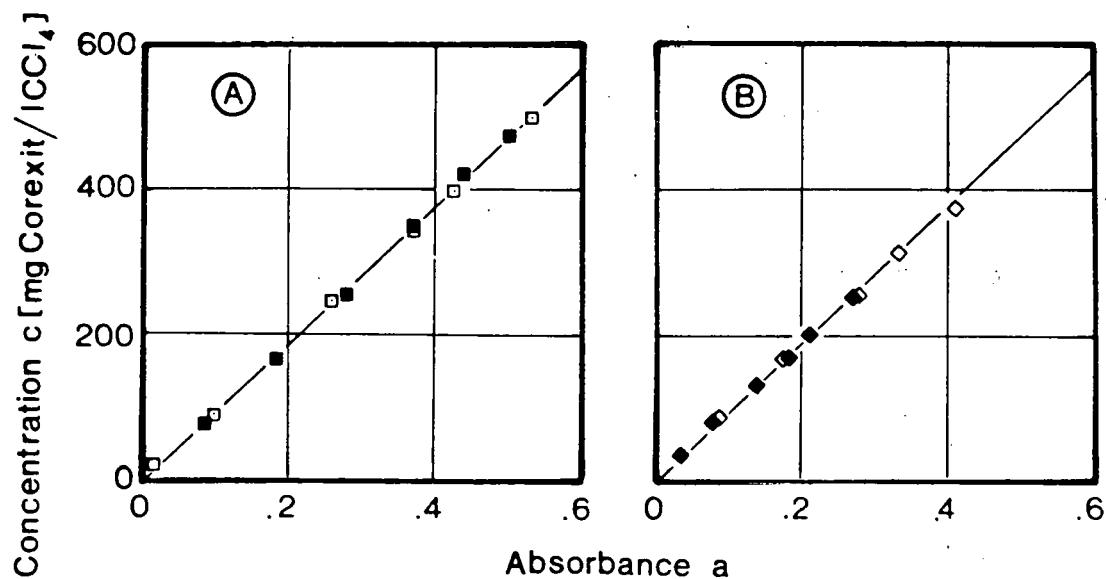


Fig. 4. Calibration curve for Corexit 9527 alone at $3600 \text{ [cm}^{-1}\text{]}$ (A)
 Mixtures compared with the calibration curve (B)

$$a = 0.00108 \quad c_C = 0.00576 \pm 0.00530 \quad (4)$$

Attention is here drawn to the fact that very high values of concentration is needed to give the desired calibration curve, and that this limits the usefulness of the present approach to cases where the concentration of Corexit in the solvent CCl_4 is high. This however is the case in the investigations where the present method is to be applied.

Now, mixtures are prepared, i.e. a mixture of known ratio Corexit/Kuwait Crude is dissolved in CCl_4 in different concentrations. When these samples are scanned at $3600 \text{ [cm}^{-1}\text{]}$ values for the absorbance is obtained and since the concentration of Corexit in the mixture is known, the results can be compared with the straight line calibration curve obtained in Fig. 4A. This is done in Fig. 4B. The accuracy with which the amount of Corexit in the mixtures is predicted by the calibration curve shows that the infrared spectrophotometer "sees" only the Corexit at the wave number $3600 \text{ [cm}^{-1}\text{]}$. One has thus a method of determining c_C in a mixture of unknown ratio.

A series of different mixtures are now prepared and scanned at $2930 \text{ [cm}^{-1}\text{]}$. The results are shown in Fig. 5 where the slope of the straight line calibration curves depend on the ratio Corexit/Kuwait Crude.

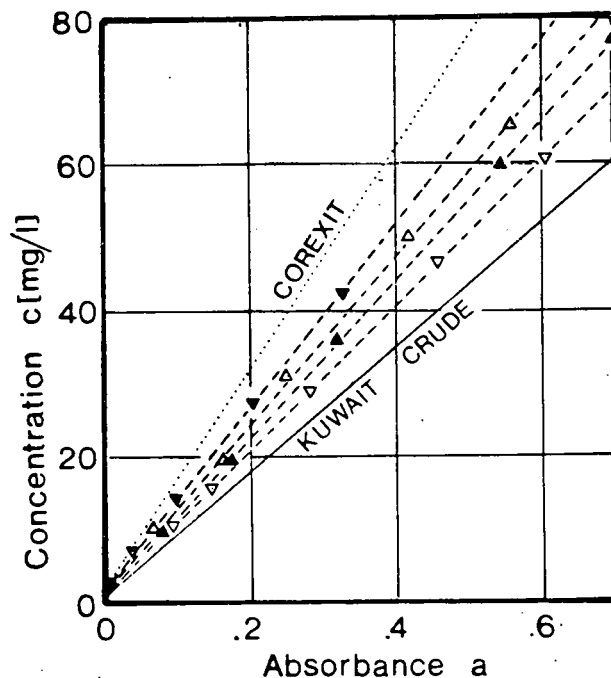


Fig. 5. Calibration curves at $2930 \text{ [cm}^{-1}\text{]}$ for different mixtures

Figure 5 also shows the previously established calibration curves for Corexit alone and Kuwait Crude alone.

One may now gather the information obtained. The concentration c_m of a mixture of ratio $r = \text{mg Corexit} / \text{mg Kuwait Crude}$ may be given as

$$c_m = c_c + c_o \quad (5)$$

and the ratio will be

$$r = c_c / c_o \quad (6)$$

The result of the scanning at $2930 \text{ [cm}^{-1}\text{]}$ may be given as

$$a = \lambda(r) c_m \quad (7)$$

where the slope λ of the calibration curve is a function of r .

This relationship is shown in Fig. 6

$$\frac{\lambda - \lambda_\infty}{\lambda_0 - \lambda_\infty} = (1+r/0.425)^{-0.75} \quad (8)$$

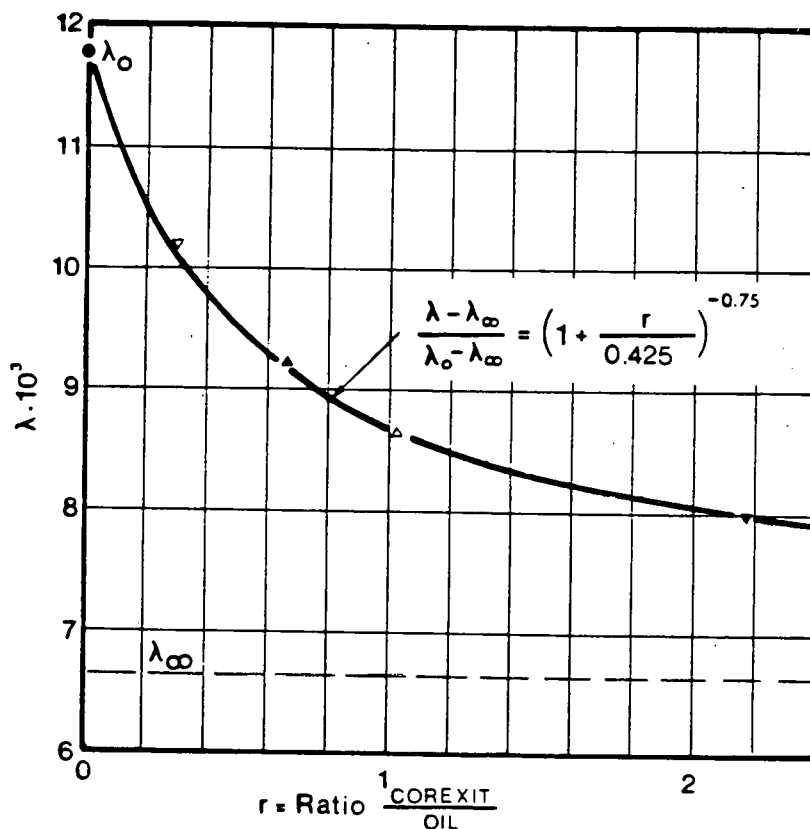


Fig. 6. The slope of the calibration curve as function of the ratio r of the mixture

where

- λ_0 = slope for oil alone
- λ_∞ = slope for Corexit alone
- λ = slope for a mixture of ratio r

This is the end result of the investigation, and it is emphasized that eq. (8) is a curve fit only and that no theoretical basis is used. It may be that it can be improved and that another expression in other circumstances may be preferable. This however does not change the fact that this investigation gives a method whereby the content of hydrocarbons in a sample can be split-up into one part originating from the dispersant and one part originating from the oil. The data used to obtain this may now be used as examples.

In Table I the measured values of c_m , c_C , c_o , a_m and $r_{meas.}$ are given. Each one of these samples may be treated as an original case

TABLE I.

Series	No	c_m [mg/l]	c_C [mg/l]	c_o [mg/l]	a_m	$r_{meas.}$	$r_{comp.}$
P2	Ba	65.51	33.15	32.36	.558	1.0244	1.060
	Bb	49.84	25.22	24.62	.419		1.083
	Bc	30.94	15.66	15.28	.248		1.174
	Bd	19.69	9.96	9.73	.163		1.111
	Be	10.15	5.14	5.01	.077		1.295
P3	Ca	76.76	29.68	47.08	.699	.6304	.644
	Cb	59.81	23.13	36.68	.545		.643
	Cc	35.98	13.91	22.07	.319		.668
	Cd	19.63	7.59	12.04	.176		.658
	Ce	9.90	3.83	6.07	.082		.735
P4	IIIa	60.58	13.88	46.70	.606	.2973	.301
	IIIb	10.72	2.46	8.26	.097		.338
	IIIc	15.73	3.60	12.13	.146		.327
	IIId	29.15	6.68	22.47	.282		.313
	IIIe	46.36	10.62	35.74	.456		.307
P5	IIa	42.77	29.28	13.49	.328	2.17	2.388
	IIb	7.00	4.79	2.21	.042		5.314
	IIc	14.41	9.86	4.55	.100		3.141
	IId	27.75	19.00	8.75	.203		2.704
	IIe	-	-	-	-		-
Pla	10	-	-	-	-	.8109	-
	11	10.98	4.92	6.06	.097		.829
	12	-	-	-	-		-
	13	22.54	10.09	12.45	.201		.816
	14	34.17	15.30	18.87	.301		.831
	15	46.17	20.67	25.50	.415		.807
	16	57.41	25.71	31.70	.530		.776
17	82.24	36.83	45.41	(.757)	-		

where only c_C and a_m are known. The value of c_o is supposedly known from scanning at $3600 [cm^{-1}]$ and a_m is the absorbance found from scanning at $2930 [cm^{-1}]$. With these two as only input data the following procedure is followed:

- 1.) An initial ratio $r=r_1$ is assumed
- 2.) Then the corresponding $\lambda=\lambda_1$ is computed from eq. (8)
- 3.) The corresponding concentration of the mixture $c_{m,1}$ is found from:

$$c_{m,1} = a_m / \lambda_1$$

- 4.) The corresponding concentration of oil is found from:

$$c_{o,1} = c_{m,1} - c_C$$

- 5.) The corresponding ratio $r_2 = e_C / e_{o,1}$ is computed
- 6.) The value r_2 is compared with r_1 . If the difference is too great one repeats steps 2.) . . . 6.) until the ratio introduced is close to the one obtained.

This procedure is used to obtain the values r_{comp} in Table I.

The procedure works very well provided:

- a.) the concentration e_C is not too low
- b.) the ratio $0 \leq r \leq 1$

How the procedure breaks down when this is not the case is well brought out by the data in Table I. The break down of the method for large values of r is of course due to the asymptotic behavior of the curve in Fig. 6.

The application of the method presented here may meet with difficulties. The use of CCl_4 as a solvent for the extraction shows that the peak at $3600 \text{ [cm}^{-1}\text{]}$ is highly influenced by water. This can be extracted, using say anhydrous Sodium Sulfate (Na_2SO_4) to "dry" the aliquot, i.e. to extract the water without seriously affecting the peaks at $3600 \text{ [cm}^{-1}\text{]}$ and at $2930 \text{ [cm}^{-1}\text{]}$ as shown by the example displayed in Fig. 7. This is however a rather time

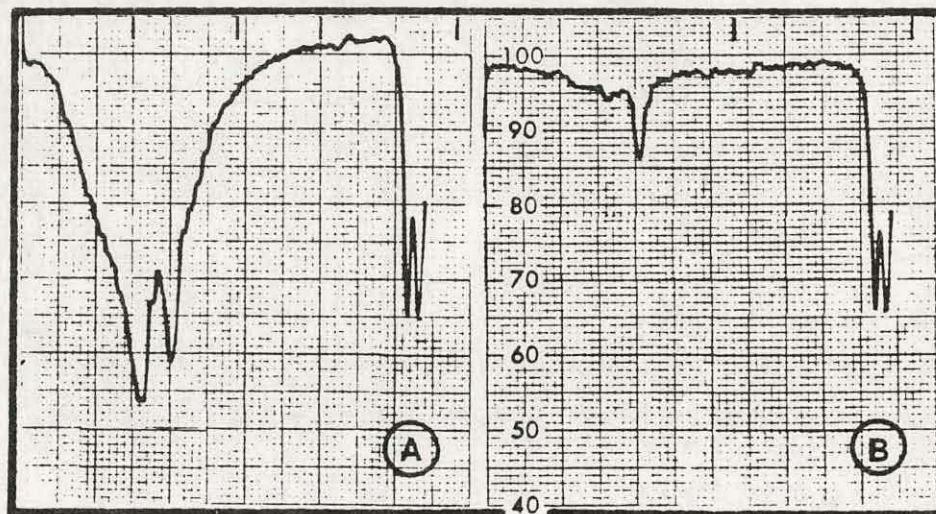


Fig. 7. The influence of water on the peak at $3600 \text{ [cm}^{-1}\text{]}$ (A) and that influence removed by Na_2SO_4 (B)

consuming procedure, and another procedure is to be suggested whereby the complications at the wave number $3600 \text{ [cm}^{-1}\text{]}$ may be avoided.

If the hydrocarbons in a sample is extracted by applying aliquots (CCl_4) of a fixed magnitude to the sample, shaking the sample and draining off the aliquot, successive aliquots will show a decreasing concentration of hydrocarbons. It turns out that when the hydrocarbons originate from crude oil, a rapid decrease in the concentration of each subsequent aliquot is observed, a situation which has been investigated in [1]. If on the other hand the hydrocarbon originates from Corexit 9527 the concentration decreases much more slowly. This is exhibited in Fig. 8 where the concentration of Corexit in the water

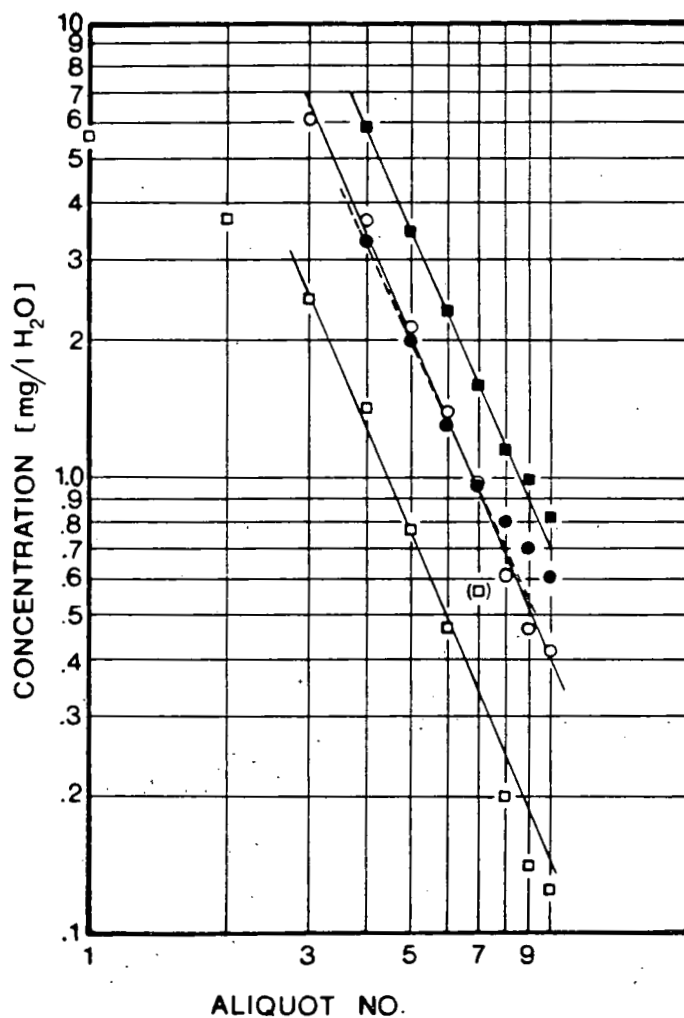


Fig. 8 Concentration $c_{C,i}$ as indicated by subsequent aliquots

sample as indicated by each aliquot is shown. The concentration $c_{C,i}$ indicated by aliquot no. i is found by means of the calibration curve in Fig. 3. For values less than 1 [mg/l H_2O] the determination becomes somewhat uncertain. It is seen that the data points indicate a relationship given by the straight lines.

$$\ln c_{C,i} = \lambda \ln i + b \quad (9)$$

For the cases shown in Fig. 8 the data are given in Table III where m is the standard deviation obtained through linear regression applied to the data points.

Table III

Legend	No.	λ	b	m	c_C [mg/l H_2O]	Aliquots used to determine line
	I	-2.349	4.493	+ 9%	49.7	all
	II	-2.200	4.235	+ 2.0%	51.2	4.5.6.7
	III	-2.334	5.012	+ 1.2%	72.8	4.5.6.7.8
	IV	-2.402	3.593	+ 8.3%	25.0	3.4.5.6

To this one may add that the first aliquots do not follow the regular behavior indicated by eq. (9). Fig. 9 reveals in Case IV that the following relation then seems to apply:

$$\ln c_{C,i} = \alpha i + \beta \quad (10)$$

where the respective values of α and β are given in Table IV.

Table IV

No	α	β	m	Computed from eqs. (11, 12, 13)		
				$e^{\alpha + \beta}$	k	c_C
I	- .4368	3.001	+ 7.0%	12.99	.646	50.3
II	- .4604	3.020	+ 3.6%	12.93	.631	48.0
III	- .4026	3.313	+ 7.0%	18.36	.669	75.9
IV	- .4508	2.195	+ 5.5%	5.72	.637	21.6

It reveals furthermore that eq. (10) can be applied with confidence also to the subsequent aliquots provided one does not go to too low concentrations.

The following additional information is important : The samples I and IV were prepared with Corexit alone, whereas samples II and III were prepared with a mixture of Corexit and Kuwait Crude in a ratio $r_{II} = 1.04$ and $r_{III} = 1.24$ respectively. Tables III and IV reveal through the values of λ and α that

- 1.) The concentrations $c_{C,i}$ of subsequent aliquots follows a "universal" law under the conditions used. This law is neither given by eq. (9) nor by eq. (10) but these equations are good approximations in two different regions.

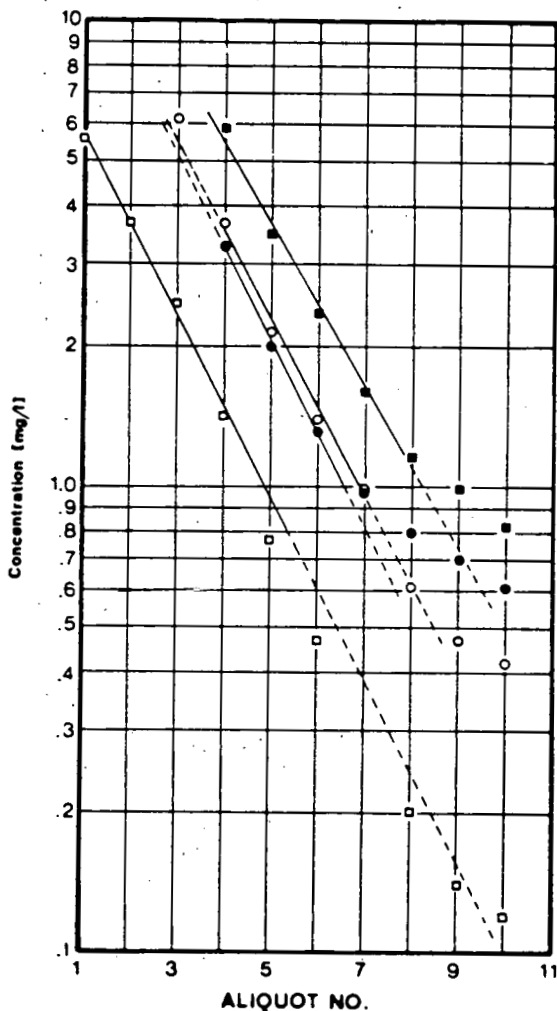


Fig. 9. Concentrations $c_{C,i}$ of subsequent aliquots

- 2.) The extraction of Corexit according to the "law" appears to be uninfluenced by the presence of oil in the sample.

This last observation gives rise to the following line of reasoning:

- A.) It is assumed that the three first aliquots (in the cases used here) contains both oil and dispersant, but that the subsequent aliquots contain dispersant alone. This is due to the different way in which oil and Corexit apparently are extracted.
- B.) The next aliquots (No. 4, 5 and 6) ought then to follow the law of eq. (10).
- C.) This law applies also to the first aliquots if the extraction takes place uninfluenced by the presence of oil.
- D.) Since the curve according to which the extraction takes place is assumed to be "universal", it is possible to compute the original concentration of Corexit in the sample based on the information obtained from aliquots No. 4, 5 and 6.

Now, if eq. (10) can be applied, it means that:

$$c_{C,i} = e^{\alpha i + \beta} \quad (11)$$

$$c_{C,i+1} = e^{\alpha(i+1) + \beta}$$

or

$$c_{C,i+1} / c_{C,i} = e^{\alpha} = k \quad (12)$$

If this was true for all aliquots, one would find the total concentration of Corexit in the sample as

$$\begin{aligned} S &= \sum_{i=1}^{\infty} c_{C,i} = \frac{e^{\alpha + \beta} (1 + k + k^2 + \dots)}{1} \\ &= e^{\alpha + \beta} \frac{1}{1 - k} \end{aligned} \quad (13)$$

Since a different "law" applies for later aliquots eq. (13) will underestimate the total concentration. One may however assume that because of the "universality" of the decay, the deviation measured in percentage is a constant. If this constant is put equal to 0.73 one will, with the values of α and β determined in Table IV obtain the concentrations computed in the same table. This shows that the method seems to work.

One final comment may be advanced. When using the method enough aliquots must be applied to secure that the oil has been removed and that one has reached that part of the extraction procedure where subsequent aliquots lie on a line with $\alpha = -0.45$ when exhibited as done in Fig. 9. In the cases on which the present method was investigated the sample size was always 500 ml and the aliquot size 30 ml. This method is used in the evaluation of the drop size as well as the rain drop experiments.

Reference

- [1] Leif N. Persen "The Entrainment of Oil from an Oil Slick into the Water Column, Workshop, Princeton, May 1979.

Appendix C: The Evaporation Tests

THE EVAPORATION TESTS

The entrainment process is to be studied experimentally by properly chosen experiments. A major feature of such experiments is the determination of concentrations of oil in samples from the water column. It has, however, been noted that a certain percentage of the oil will evaporate and not be entrained in the water column over a longer period. This has led to the study of the evaporation process. Both Kuwait Crude and Corexit 9527 have been tested by letting an open surface of the two fluids be exposed to wind in a wind tunnel where the velocity field could be monitored. In addition to the tests with the two fluids alone, tests were made to investigate the mixtures of Kuwait Crude and Corexit 9527 in the ratios 20:1, 10:1, 7:1 and 5:1. Both for the case of Kuwait Crude alone, as well as for mixtures of Crude and Corexit 9527, the influence of an underlying waterbed was examined.

It should be realized that crude oil in general consists of components which evaporate differently. Thus, under given conditions only a portion of the crude oil will evaporate, whereas Corexit 9527 resembles water in the sense that it almost evaporates entirely under the same conditions. The results may thus not be expected to be comparable.

The physical quantities involved in the tests are the following:

m_e = mass of the evaporated portion of the fluid

m = total mass of the fluid used in the experiment

t = time

U_s = slip velocity in the air at the interphase (Fig. 1)

$du/dy|_{y=0}$ = velocity gradient in the air at the interphase (Fig. 1)

ρ = density of the oil

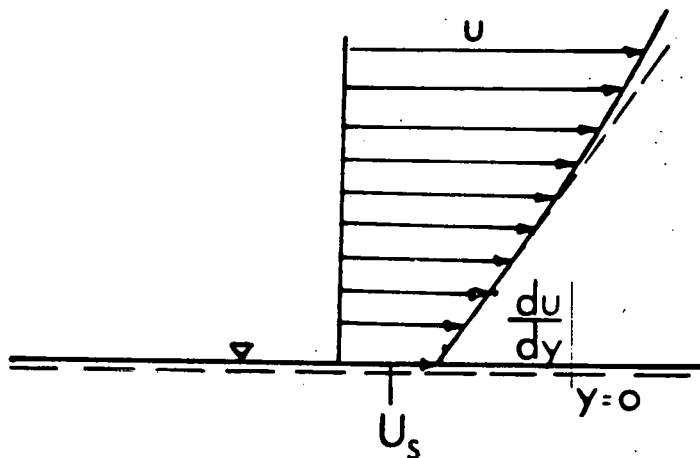


Figure 1. Velocity profile above the fluid

h = depth of the oil (oil slick thickness)

Buckingham's Π - theorem indicates the outcome of the experiment to be expressible in terms of the following variables:

$$p = \frac{m_e}{m} = (\text{percentage evaporation})$$

$$\tau = \frac{U_s t}{h} = \text{dimensionless time}$$

$$\Pi_1 = \frac{h}{U_s} \cdot \left. \frac{du}{dy} \right|_{y=0}$$

$$\Pi_2 = \frac{\rho h^3}{m}$$

This means that the result of the experiments ought to be expressible as:

$$p = \frac{m_e}{m} = F \left(\frac{\rho h^3}{m}, \frac{h}{U_s} \left. \frac{du}{dy} \right|_{y=0}, \frac{U_s t}{h} \right)$$

Table I shows the value of the parameters for six different tests performed with Kuwait Crude Oil. The results from these tests are shown in Fig. 2 where p is plotted as function of τ . They show that p is only slightly dependent on Π_1 and Π_2 which reflects the fact that the exposed surface as well as the depth of the fluid (oil slick thickness) was kept almost constant. In order to get an

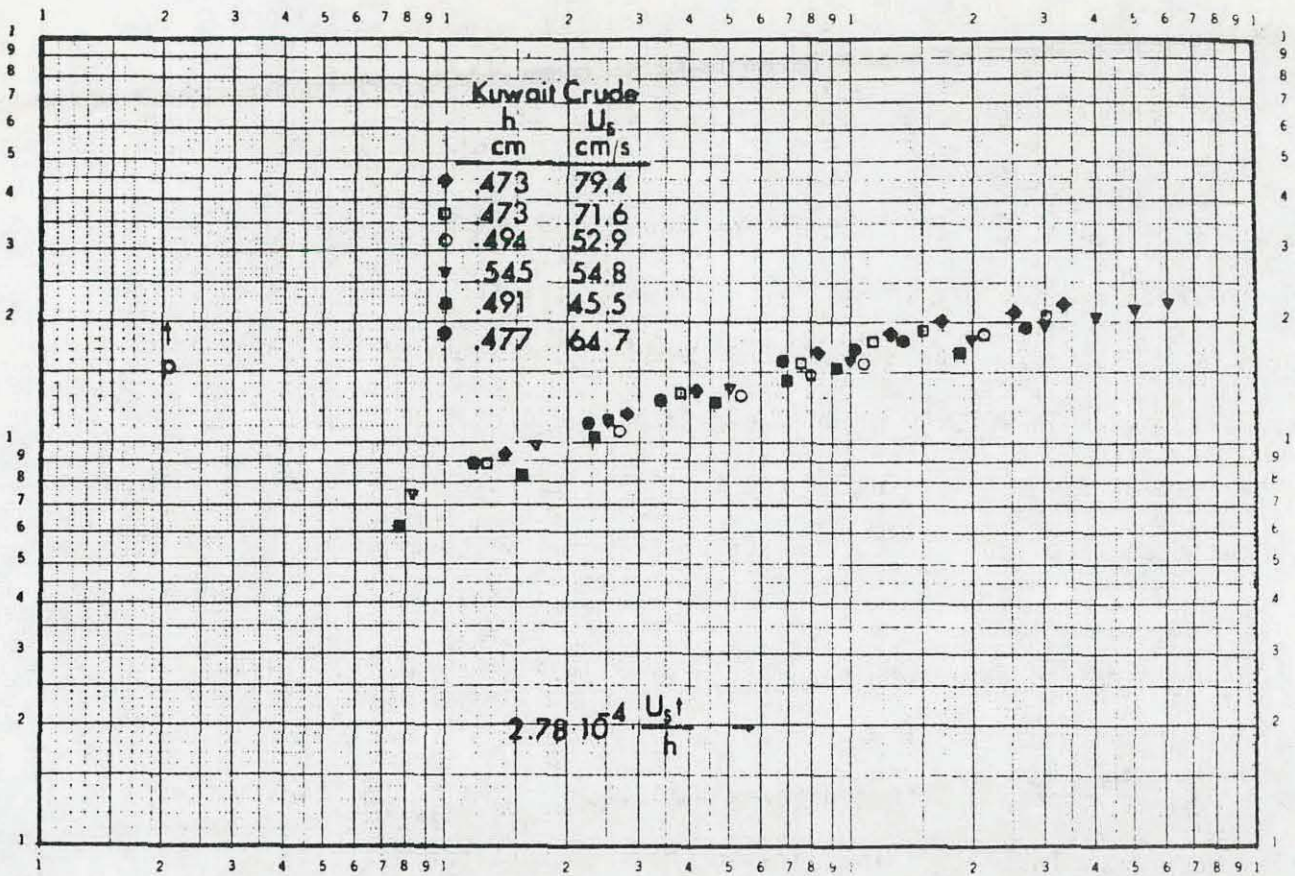


Figure 2. Evaporation data p versus U_s t/h

TABLE 1 (KUWAIT CRUDE OIL)

No.	Leg.	U _s [ft/s]	du/dy _{y=0} [1/s]	h [cm]	U _s /h [1/s]	$\frac{\pi_1}{U_s} \frac{du}{dy} \Big _{y=0}$	$\pi_2 \cdot 10^3 =$ $\rho h^3 / m \cdot 10^3$
1	○	1.7344	4.38	.494	107.01	.04093	.7211
2	■	1.4932	4.74	.491	92.69	.05114	.7124
3	●	2.1228	7.56	.477	135.65	.05573	.6723
4	□	2.3480	12.00	.473	151.30	.07931	.6611
5	▽	1.7982	8.76	.545	100.57	.08711	.8777
6	◆	2.6064	8.28	.473	167.96	.04930	.6611

indication of the asymptotic value of p , the following curve was fitted to the data:

$$p = \frac{A(\tau/\tau_0)^\kappa}{1 + (\tau/\tau_0)^\kappa}$$

where $\kappa = 0.75$ and $\tau_0 = 26.78 \cdot 10^2$. The asymptotic value $A = 26.00$ is found from the data and the way in which the curve represents the data is exhibited in Fig. 3. This result should be considered in the light of an evaporation test performed in a ROTOVAP at 40°C over a period of 24 hours which led to a weight loss of 32.3%. In view of the fact that the present results were obtained at a temperature of $20 - 22^\circ\text{C}$, the agreement between the experimental results seems reasonable.

The evaporation data obtained for Corexit 9527 alone and for different mixtures of oil and Corexit are shown in Figs. 4 and 5. For Corexit alone, the data have been obtained with a greater variation in the fluid thickness as is easily seen from Table II. The data do, however, not correlate as well with only non-dimensionalizing the time and introducing τ as is seen from Fig. 4.

This may partly be due to the fact that different trays were used and certain cases where the surface area changed due to evaporation. For the mixtures, however, this did not happen, and the data correlate well again.

The importance of these tests does not lie so much in the actual results which, for Kuwait Crude, show that $\sim 75\%$ of the total evaporation caused by

Table II (Corexit 9527)

No.	Leg.	U_s [ft/s]	$du/dy _{y=0}$ [1/s]	h [cm]	U_s/h [1/s]	$\frac{\pi_1}{U_s} = \frac{h}{U_s} \cdot \frac{du}{dy} _{y=0}$	$\pi_2 \cdot 10^3 = \frac{h^3}{\rho h^3/m} \cdot 10^3$
8	□	2.4912	10.74	.561	135.35	.07936	.9300
9	●	1.8900	6.48	.768	75.01	.08639	1.7429
10	◆	2.4670	10.50	.378	198.93	.05278	.4222
11	■	1.5056	4.02	.513	89.46	.04494	.7776
12	◇	2.6016	10.62	.457	173.52	.06120	.6171
13	▼	.426	14.10	1.698	7.65	1.84388	3.1622
14	▲	.144	15.30	1.731	2.54	6.03408	3.28631

wind under the circumstances investigated has taken place when

$$\frac{U_s t}{h} = 12 \cdot 10^5$$

i.e., for circumstances investigated here approximately after two hours. It is far more important for the study of the entrainment process to realize that the composition of the entrained oil differs due to weathering.

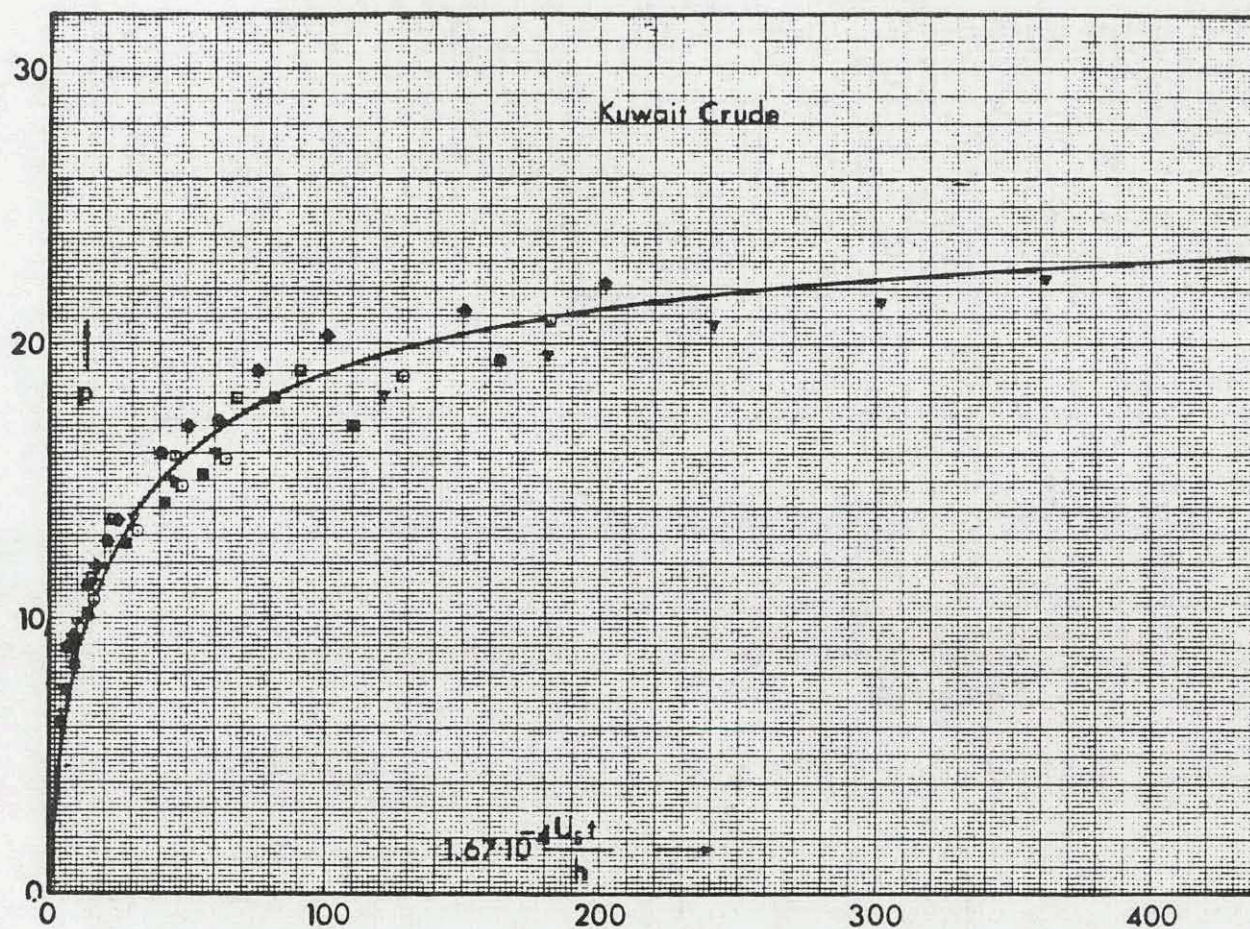


Figure 3. Evaporation data p for Kuwait Crude exhibiting the asymptotic value $p = A = 26.0$

Table III (Kuwait Crude: Corexit 9527)

No.	Leg.	U_s [ft/s]	$du/dy _{y=0}$ [1/s]	h [cm]	U_s/h [1/s]	$\frac{\pi_1}{U_s} = \frac{h}{U_s} \frac{du}{dy} _{y=0}$	$\pi_2 \cdot 10^3 = \frac{h^3}{\rho} \frac{du}{dy} _{y=0}$	Mix:
15	◆	2.3496	11.52	.438	163.51	.07046	.56688	20:1
16	◇	2.3184	11.58	.440	160.60	.07210	.57207	7:1

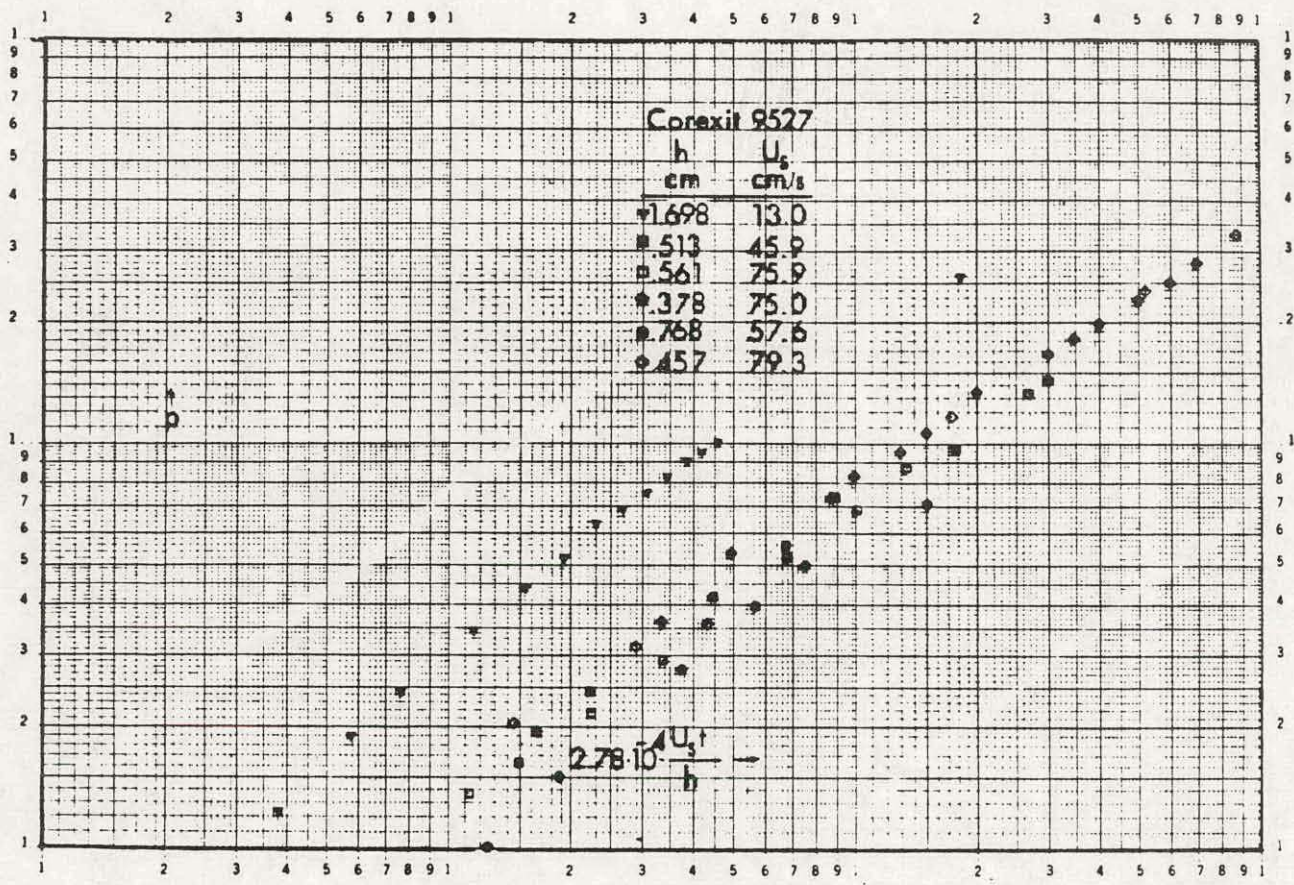


Figure 4. Evaporation data p versus τ for Corexit 9527

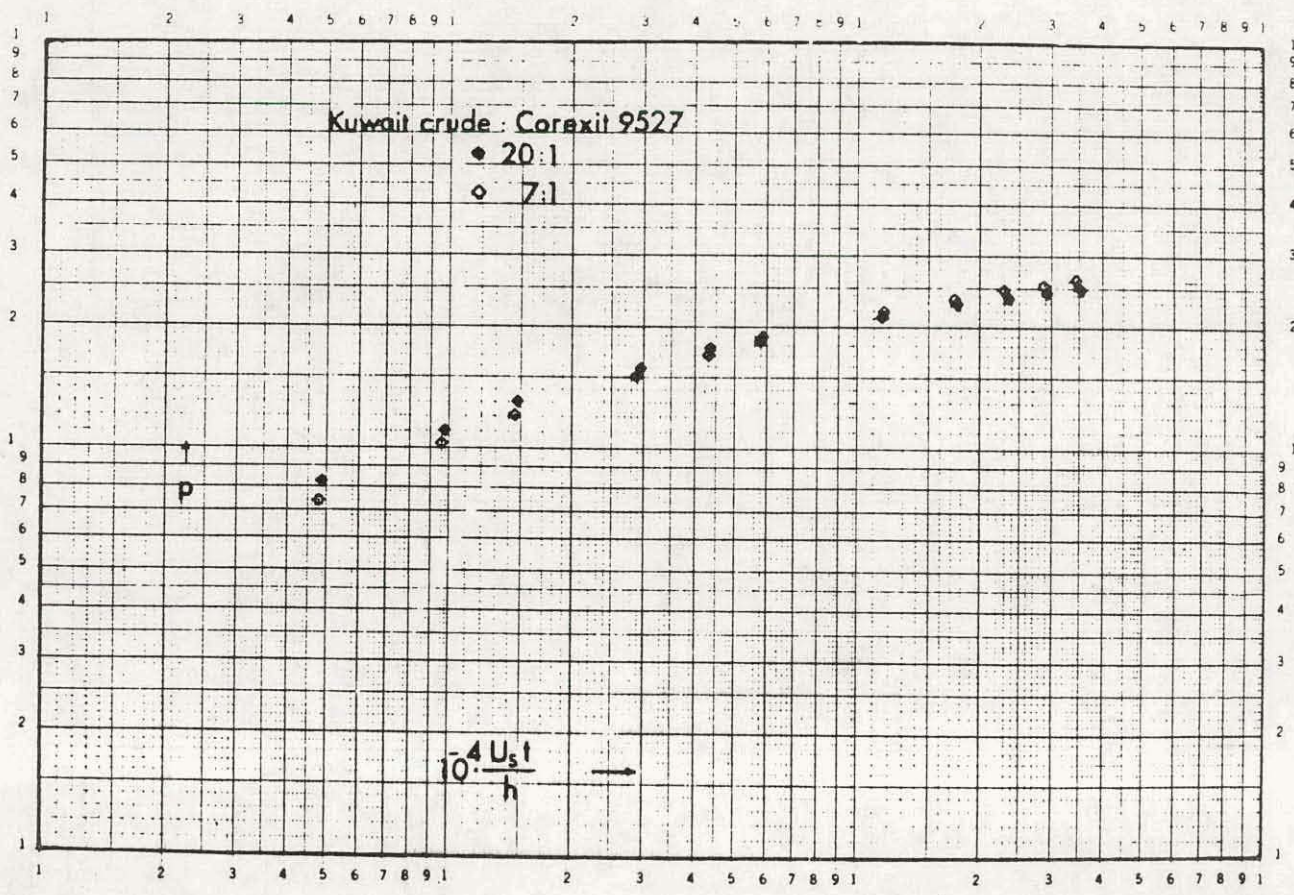


Figure 5. Evaporation data p versus τ for mixtures of Kuwait Crude and Corexit 9527

12.3 Section 5 Computer Manual
URF Oil Spill Model

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CHAPTER I INTRODUCTION

This manual is a guide to Version 2 of the URI Oilspill Model. The model, although it treats most of the known processes involved in the fate of spilled oil, has been designed primarily to study cleanup and treatment alternatives for a given spill condition. This requires that input be easily entered and output easily obtained in the shortest amount of time. The model has also been designed to allow for the rapid implementation of new modules reflecting advances in the state-of-the art.

The computer code is currently implemented on an Intel Advanced System/5 which is functionally compatible with an IBM System 370. It is written in Fortran IV and is run as a batch job. The main program, as presently configured, requires about 465 kilobytes of memory to run and a typical job using 2000 marker particles, 30 spilletts and a time step of one day, consumes about 16 CPU minutes for a 72 day simulation.

In the next section of this chapter, an overview of the various steps required for a complete simulation are briefly described.

Chapter II is devoted to the input programs used to format environmental data for input to the preview and full scale simulation. The function of the preview run is discussed in Chapter III while the general operation of the complete simulation is outlined in Chapter IV. Chapter V provides a brief summary of the output programs used to plot the results. The details of the various programs as well as how to set up a complete simulation is covered in the appendices. In particular, Appendix I covers input to the preview and complete simulation model; Appendix II, the output available from these models; Appendix III a description of all variables contained in common in the simulation model; Appendix IV, a detailed description of the operation of each subroutine of the model; Appendix V a similar description for the input programs; Appendix VI a detailed description of the output programs; Appendix VII a listing of all programs; Appendix VIII output from a sample run; and Appendix IX a summary of oil properties required for input.

OVERVIEW

The simulation of an oil spill is divided into four steps. Formation at input, data, spill preview, main simulation and output. The flow chart showing this process is presented in Figure 1.

As indicated in Figure 1, the user may elect to prepare all input data with or without the use of the input programs. These programs manipulate only the most complicated input data, the environmental variables (bathymetry, wind, current, etc., see Chapter II), one of the five major input groups. The remaining four groups are discussed in greater detail in Appendix I. There are two characteristics of the environmental data which render them more complicated than the other input data. First, they read into the main program on grids defined by:

1. The grid origin in longitude and latitude.
2. The spacing of grid elements.
3. The number of elements in x and y.
4. The angle the grid makes with lines of constant latitude.

OVERVIEW

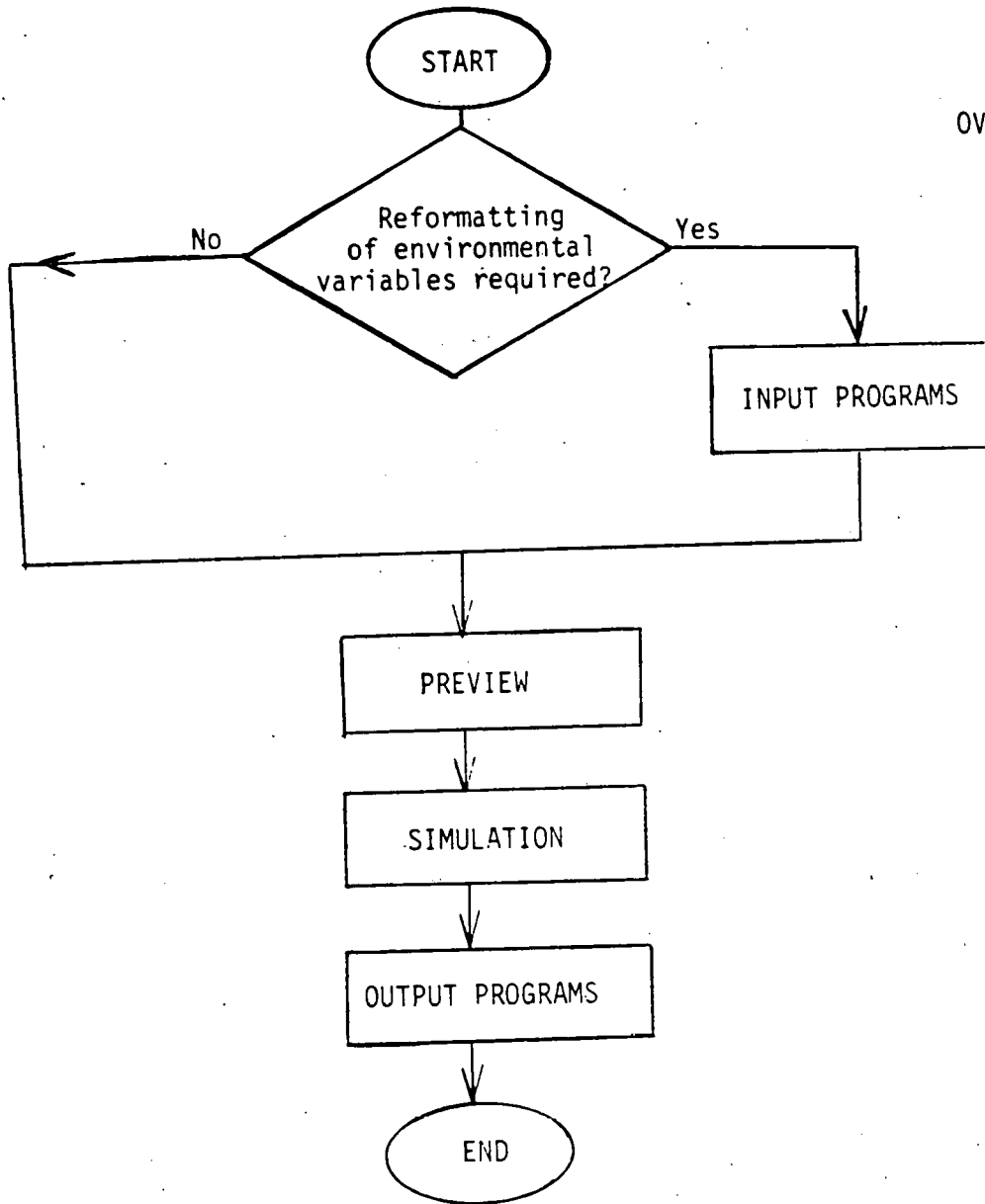


Figure 1. OVERVIEW

Second, the spacing of grid elements may be in meters or degrees longitude and latitude. These alternate grid spacings permit the model to operate on one of two size scales but also increases the complexity of defining the values of the variables and the grids. In the small scale mode, horizontal distance calculations are performed in meters while in the large scale mode, the calculations are performed in degrees. This allows environmental data to be obtained from satellites, where the data locations cover a spatially large grid requiring spherical coordinates such as longitude and latitude, or from smaller scale data collection programs such as might be located nearshore with recording instruments located only a few kilometers apart.

The input programs may be used to format the environmental variables to input the simulation model and/or to check the environmental data sets. Even if the user prepares the environmental data sets, the use of the input program that verifies the format is suggested. A small error in the location or format of an environmental grid may result in a costly but useless run.

In order to understand the second step in the simulation process, the preview run, it is important to first understand the difference in the concentration in the model of oil on the surface of the water compared to that of oil entrained into the water column. The surface oil is treated as a collection of "spillets." These are circular puddles of oil which spread, drift, evaporate, etc., independently of all other "spillets." If they overlap by more than predefined fraction, they are combined into one larger "spillet." The parameters describing this larger "spillet" are determined either by the sum of the corresponding parameters of the small "spillets" (such as the total volume of oil) or by the weighted sum of those parameters (such as the center of the "spillet"). In the present configuration, up to one hundred "spillets" are allowed at any one time. Oil is added to a spillet either from a source or by adding spillets together when they overlap. Table 1 gives a description of the variables used to define a "spillet."

The subsurface oil is treated as a collection of droplets each of which represents a large number of droplets with similar properties. The droplets in the model are, therefore, part of a statistical representation of the actual dispersion. Each droplet is described by a set of parameters such as the droplet radius, entrained mass associated with the droplet, its location, etc. These parameters are listed in Table 2. Up to two hundred categories of droplets are currently allowed. There may be many droplets in each category, but the total number of droplets is limited by memory requirements (to 2000 at present) and by execution time. A neutrally buoyant droplet may be used to represent the dissolved portion of the spilled oil.

Those subroutines that deal with the surface oil are formally separated from those dealing with the subsurface oil everywhere except in the determination of the volume of entrained oil, as the number of entrained marker particles. The preview run executes only the surface routines and keeps a running tally on the mass balance. It is used primarily to determine the mass to be associated with each subsurface particle. Such a determination is extremely difficult without this intermediate step because the total entrained mass depends on the wind

TABLE 1

"SPILLET VARIABLES"

- Area of spilllet treated thus far (meters²).
 - Density of oil currently in spilllet (gm/cc).
 - Fraction of each of up to eight classes.
 - Radius of Spillet (meters).
 - Interfacial tension of oil prior to treatment (Dynes/cm).
 - Interfacial tension of oil after chemical treatment (Dynes/cm).
 - Kinematic viscosity of the oil (Centistokes).
 - Mass of oil remaining in Spillet (metric tons).
 - Longitude and latitude at the center of the spilllet.
-

TABLE 2

PARAMETERS OF DISPERSED OIL DROPLETS

- Radius of the droplet (mm).
- Density (gm/cc).
- Fraction of each of up to eight classes of hydrocarbons.
- Mass of entrained oil represented by the given droplet.
- Longitude, latitude and depth in the water column (m) of the droplet.

speed as a function of time, the age of the oil, spill surface area, etc. If the number of particles is to be fixed, say at 2000, a good estimate of the total entrained mass is required to allocate the correct amount of mass to each entrained particle.

In addition to providing the user with an appropriate estimate of the mass associated with each entrained particle, the preview run is also useful in providing a preview of the surface behavior of the spill. Memory requirements may be less than for the full simulation and the time of execution is greatly reduced.

The main program integrates the subsurface portion of the simulation into the model.

The surface processes included are drifting, spreading and deposition. The oil enters the water column by dissolution and entrainment. The algorithm for the subsurface diffusion and advection makes use of the particle-in-cell method and is described in detail in Pavish (1977) and Spaulding (1976).

The output of the main program includes spill size and location, subsurface concentrations, particle positions and a mass balance. In the final step of the simulation, this output is presented in graphical form by the various plotting routes. Specifically, mass balance, areal extent of the oil and a vertical view of the spill area are plotted.

CHAPTER II ENVIRONMENTAL GRIDS AND INPUT PROGRAMS

Input parameters required by the preview and the main simulation are logically divided into five main categories: environmental, oilspill, treatment, run control, and restart. Each of these categories has associated with it a well-defined format or set of formats. The user is required to determine and properly format variables in the first four groups. The restart data set is generated by the main simulation and intended to be transparent to the user; hence, only its function is described in this chapter.

The most complex set of input parameters is the environmental data set. In light of this, a pair of programs was written that will place environmental data into the proper format for input to the simulation model or check the environmental grids that may have been generated by the user. In this chapter, these programs are briefly described. Prior to this description, however, it is necessary to introduce the concepts associated with the environmental grids. This is done in the first section, the second section being reserved for the program description.

The other input parameters and formats are discussed in detail in Appendix I along with a list showing the order of entry of all input data.

A. Environmental Coordinate System

The environmental data are entered on a set of rectangular grids. The position of the (1,1) element is used to locate the grid with respect to longitude and latitude. The spacing between values is constant but not necessarily the same in both directions. The angle of the grid with respect to lines of constant latitude is a variable, defined by an input parameter and measured counterclockwise to the X axis. The model coordinate system is right handed with, for the zero rotation case, positive x eastward, and positive y northward. A grid may consist of from one element, in which case the variable defined is assumed to be spatially homogeneous over the entire ocean, or as many as 30 x 15 elements. The environmental data can be defined by either one or two grids. For example, wind velocity has x and y components and, therefore, needs two grids. Table 3 outlines the environmental grid variables and units.

The user has the option of spacing the environmental grids either in a spherical coordinate system or in a rectangular coordinate system. Spherical coordinates are used when the spatial scale of the problem is large, i.e. during the course of the simulation, the spill is expected to drift and spread over a distance covering several degrees latitude or longitude. This is referred to as the "large scale mode." Rectangular coordinates are used when the scale of the problem is small, less than a degree or so of latitude. This is referred to as the "small scale mode." The parameter ISCAL is used to specify the scale mode and applies to all environmental grids for a given simulation.

The units of the spacing between grid elements are dependent on the scale mode chosen. Environmental grids in the large scale mode may not be rotated. The spacing for the large scale mode must be in degrees of longitude and latitude for the x and y directions respectively, the units for the tidal currents must be degrees/sec for the large scale mode

TABLE 3 ENVIRONMENTAL GRID DEFINITION

GRID	TITLE	VARIABLE 1	VARIABLE 2	FORMAT	COMMON BLOCK	COMMENTS
		Units	Units			
Bathymetry	Bathymetry	Depth Meters	- -	Real	DPTH	Must not be moved during a run
Computational Cell	Comp Cell	- -	- -	Integer	COMP	Describes operational Area- Must not be moved during a run
Temperature	Temperature	Temp. Degrees C		Real	TMPC	
Wind Velocity	Wind Vel	U m/sec.	V m/sec.	Real	WIND	
Sea State	Sea State	Height meters	Period Seconds	Real	SEAS	
Current	Utid Current	U m/sec. or deg/sec.		Real	TIDE	If large scale mode - use degrees/sec.
Current	Vtid Current	V m/sec. or deg/sec.		Real	TIDE	Same

because of the linear interpolation techniques which are used in the sub-surface portion of the model. The units of the spacing for the small scale mode is meters.

All of the grids are self-explanatory with the exception of the computation cell grid. This grid assigns an integer value to each element which when taken together, describe the area of interest (see Table 4) in both the horizontal and vertical directions. The program assumes the water surface cell reflects the particle downward and the bottom cell deposits the particle.

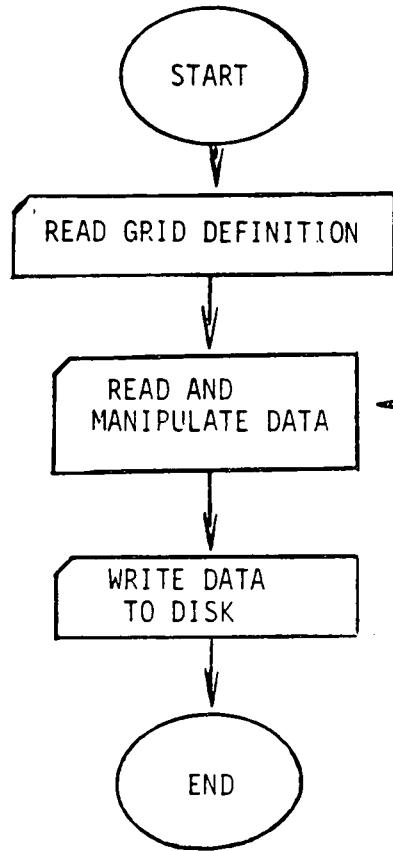
The user must change 2 lines in the subroutine BOUNV (see Appendix IV) if another value is preferred.

The gridding system is a semispace-staggered system in that the computational cells are defined in the center of a cell while the remaining grids are defined at cell corners. There are no values at any of the zero locations (i.e., (0,0), (0,1)...) for any of the grids. The depth grid and computational cell grid are not to be moved or changed during a run because the program uses these grids as references. All other environmental grids may be moved or changed in any time step.

B. Input Programs for Environmental Data Grids

As is apparent from the description above, there is a great deal of flexibility in the nature of the environmental grids, the input format required of these variables by the input subroutine ARAYIN in both the preview and main simulation models is, however, quite precise. For this reason, a pair of programs (GRIDS and READATA) have been written to aid in the preparation of environmental data and to check the data sets once prepared prior to submitting a lengthy simulation. As indicated in Figure 1, this step is not mandatory but rather included as an aid in data preparation for the user. It should be stressed that these programs operate only on environmental variables. It is also important to note that although a user may elect not to use the formatting program, GRIDS, s/he is still advised to use the program, READATA, which reads and displays the "correctly formatted" variables, i.e., to check the data sets no matter how they are prepared. An error on the input environmental data sets may result in a significant loss of time and money. Flow charts for both programs are shown in Figure 2. The first program, GRIDS, places the environmental data into the power format for use by the main program. It first reads the grid definition variables such as angle and grid spacing. The program then calls a subroutine supplied by the user. This routine must read the environmental data and then perform any necessary interpolations or conversions to put it into a rectangular grid which will be used by the main program. The program then uses the subroutine ARAYOT which is basically a copy of the subroutine ARAYIN in the main program which reads the data, the only change being that this subroutine writes instead of reads the data. GRIDS may also be used to print the data if desired. It requires 200 kilobytes of memory and takes approximately 1.5 equivalent CPU minutes to write 135 environmental grids. These storage and run values will vary as a function of the amount of manipulation required.

PROGRAM GRIDS



← USER SUPPLIED SUBROUTINE

PROGRAM READATA

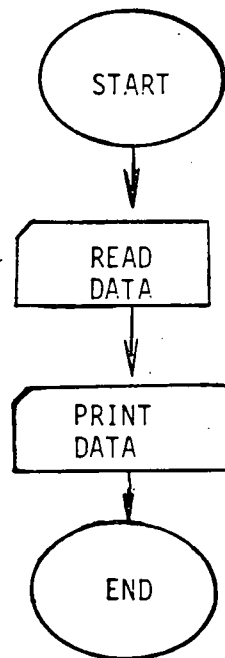


Figure 2. Flow charts for GRID and READATA

The second program, READATA, reads environmental grids as formatted for input to the simulation program exactly as the main program will read them and then prints out these arrays. This program needs only 128 kilobytes of memory and takes approximately ten seconds of execution time to read and write 75 steps.

TABLE 4
COMPUTATIONAL CELL DEFINITION

VALUE	DEFINITION	COMMENTS
0	Land cell; More than half the cell is land	Important for Shoreline Inter- action Processes
1	A water cell; Surrounded on all sides by other water cells	
2	Open Boundary cell; At least one side is at the edge of the grid	Important for inter- polation when oil tracks near the boundary.
101	Adjacent Water Cell; At least one side is connected to an open boundary cell on a land cell	Same as above
3	Reflection cell; Reflects droplets away from bottom or surface in vertical direction	
4	Bottom Depositional Cell; absorbs any oil which moves to within 1/2 grid spacing of bottom	

CHAPTER III PREVIEW RUN

In early applications of the model, it was found that prior to a full scale simulation, it was often useful to perform a quick simulation, skipping the detailed modeling of the subsurface portion of the spill. These runs were performed for one of two reasons:

1. The distribution of the subsurface portion of the spill was of little or no interest for the case under study.

2. Such a run was useful in determining the mass, XMSPAR, to be assigned to the marker particles, in the full scale simulation. As indicated in Chapter I, the total volume of oil entrained depends on a number of parameters that are continuously changing during a simulation; hence, this is a very difficult parameter to predict prior to the simulation. To make full use of the resolution offered by the subsurface portion of the model, the user generally wants to use as many marker particles as allowed, 2000 as presently configured. To do this, the correct mass per particle, XMSPAR, to achieve full utilization, must be determined prior to the simulation. If the mass per particle is too large, then less than the permissible number of marker particles will be released. If XMSPAR is too small, the entrainment of oil into the water column will terminate prematurely because there will be no particle locations available in the model to allow for the entrainment of new particles.

Because of the apparent need for such runs and the substantial savings in execution time that resulted from skipping the sophisticated subsurface portions of the model, the Preview run was introduced. The Preview run is invoked by setting the run control parameter, NRUN, to 1. The preview flow chart is shown in Figure 3 and a comparison with the flow chart for the full scale simulation shown in Figure 4 indicates that the only difference between the two runs is omission of the subsurface portion of the spill in the preview.

The output of a preview run may be used as input to the plotting programs exactly as the output from a full scale simulation, with the single exception that the subsurface distribution of the spill not be specified. The surface distribution is correct, identical with that resulting from a full scale simulation. The mass balance is correct except that droplets are not removed from the water column, so that the fraction of droplets that are deposited on the bottom or that escape through an open boundary, i.e., that leave the water column are not currently specified.

For a more detailed description of algorithms used in the surface related portion of the spill, the reader is referred to the discussion of the full simulation in Chapter 4.

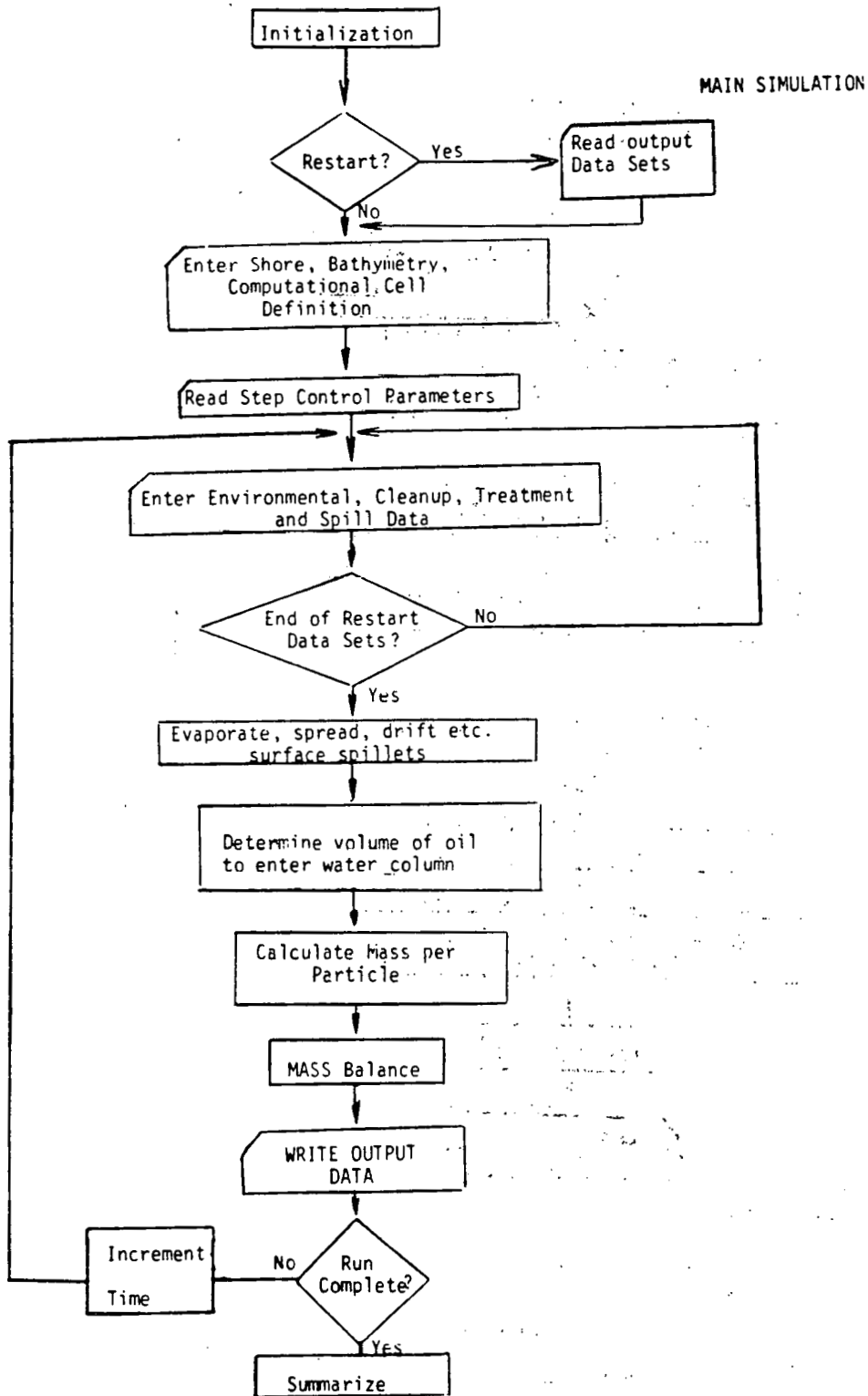


Figure 3. Flow Chart for the Preview Run

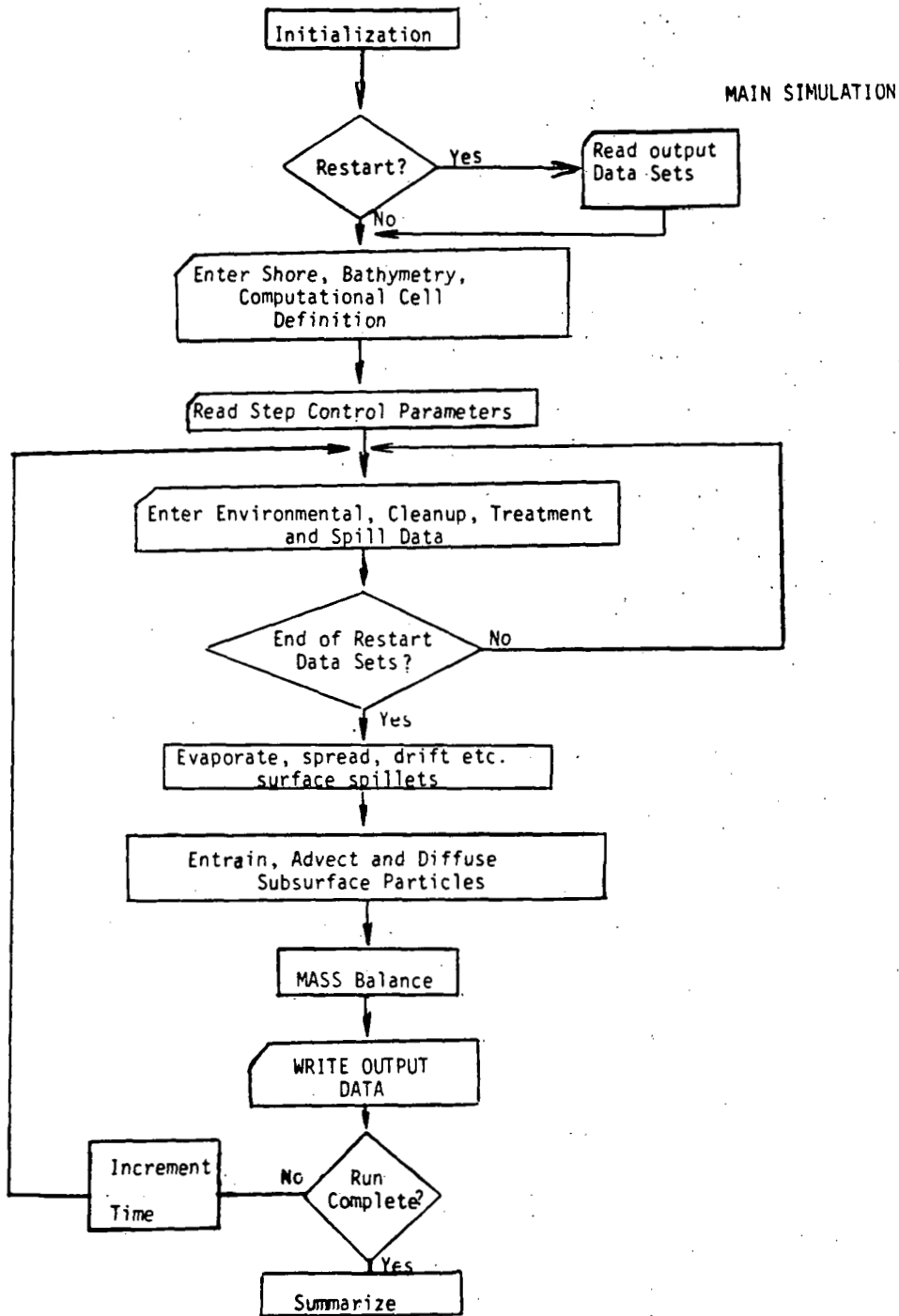


Figure 4. Flow Chart for Main Simulation

CHAPTER IV. MAIN SIMULATION

A. Introduction

This section is concerned with the description of the oil spill simulation model. The theoretical background is briefly discussed, followed by a description of program functions.

The objective of the model is to perform an environmental assessment of the treatment, with chemical dispersants, of spilled oil. This model, therefore, is directed primarily at the operational category of models dealing with cleanup and treatment alternatives. The model emphasizes the subsurface transport of spilled oil in much greater detail than those previously constructed because the major result of chemical treatment is to disperse the spilled oil into the water column. The flow chart for the model is shown in Figure 4. Most processes are handled in individual subroutines so that new algorithms can be easily incorporated. A more detailed description of the program, its subroutines and variables, are included in the Appendices III and IV.

B. Initialization

The first function performed in a simulation is to initialize. This consists of zeroing a number of counter and variables, such as mass balance, in addition to entering all fixed run control input which to a large extent will define the course of the simulation. The distinction "fixed" used above designates run control parameters that are entered once and remain unchanged for the rest of the simulation. They comprise two groups of variables, those entered in the main program which control the overall simulation (number of time steps, device numbers from which environmental data is to be read, etc.) as well as the parameterization of all surface related phenomena and those which determine the parameterization of the subsurface phenomena. All input parameters, associated formats and the order in which they are input are described in detail in Appendix I.

If this run is to continue a simulation begun in a previous run, the next step is to read the restart data set. The parameter NSTRT is used to specify a restart, being 1 if it is a continuation and 0 if the run is to begin from scratch. NSTRT equal to 1 requires that a previous run output all of the restart variables to disk. The restart data set contains the variables which define the spill at an instant in time with such as the spill size and location, droplet properties and location, mass balance and any ongoing cleanup or treatment efforts at that step. It also retains the print parameters which control the output data stream, how much output and where it is to be written. For a restarted run, the program will also read all of the stored output data sets up to the restart step. This permits the use of the original output data sets.

The program then reads the bathymetry and computational cell grids as well as the shoreline data points. Because the droplet positions are defined with respect to the bathymetric grid, this grid cannot be changed in the middle of a run. This is why these grids are read prior to the commencement of the iteration in time.

The iteration in time now begins. The first function performed at each time step is to read in the step control parameters. These parameters indicate whether or not new environmental, spill or cleanup response data are to be input in this time step. Any of the environmental or spill control data sets except the definition of computational cells, the bathymetry and the shoreline, wind, temperature, sea state, tidal velocity, mechanical cleanup efforts, chemical treatment efforts and newly spilled oil may be read in at any time step. Cleanup and treatment efforts can overlap in time and space and grids can change orientation and spacing from one time step to the next. This allows for easy insertion of different resolution data such as from two satellites with different spatial resolutions or different orbital inclinations.

If this is a restarted run, and the previous run ended on an error, the program enters at this point a loop which reads all of the control parameters, environmental grids and cleanup/treatment efforts up to the point where the previous run stopped. Normal termination at a run also results in the appropriate data being written to the restart data set. The user must specify if the restarted run is to use the previous output data sets or use a new group of data sets. This is done by the use of the parameter NSTFN. This parameter indicates whether to use the previous data sets (NSTFN=1) or to use new data sets (NSTFN=0). The user must, however, in this case supply new input and output data sets.

C. Surface Processes

The program then executes the algorithms dealing with the surface related processes (see Figure 5). Each process is dealt with by a different subroutine and all are called from one subroutine. This subroutine loops over all spilletts performing all surface related computation on one before moving on to the next. If a spillet moves to the edge of the study area, it is taken out of the loop so that no further processes will affect it. The first surface processes dealt with are those related to cleanup or chemical treatment efforts on the spillet. The variables used for this, such as efficiency, dispersant rate, etc., have been obtained through input and are described in Appendix I. These efforts are executed in the subroutines TREAT and CLNUP (see Appendix IV for a description).

The spillet is then located within each of the environmental grids. This is done for two reasons. First, it determines if the spillet is within the grid. If the spillet is outside of one grid, it is considered to be out of the study area and it is removed from the loop. If the grid is a single point, it covers the entire two dimensional plane and the spillet will never leave this grid. Second, the environmental variables are averaged over the spillet. This is done by averaging the values at all of the grid locations that the spillet covers. Some values such as depth are not used currently but the average wind velocity is used for evaporation, entrainment and drifting and the average current is used for drifting. See subroutine LOC8 in Appendix III for a detailed description of the location procedure.

The natural entrainment of mass and the creation of marker particles, is performed next. The amount of naturally entrained oil is determined from the Audunson et al. (1979) formulation. An exponential decay is added to Audunson's model to simulate the decrease in the amount of oil

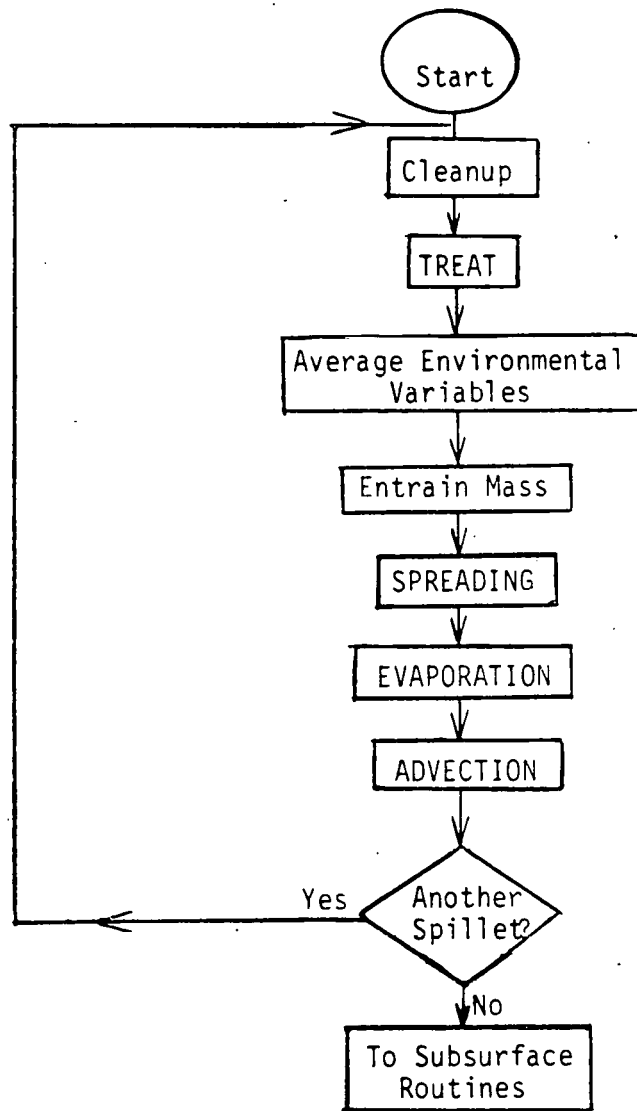


Figure 5. Flow Chart for Surface Portion of Simulation

entrained due to weathering. See subroutine ENTMAS, in Appendix IV, for a detailed discussion of this calculation. The amount of mass naturally entrained is combined with the mass dispersed into the water column during chemical treatment and the number of particles created is determined by dividing the entrained mass by XMSPAR, the mass per particle, a user supplied parameter (see Appendix I). The particles are then distributed in an ad hoc manner (described in the Appendix IV) by subroutines ENTRN and INJECT. Grossly they are distributed at random beneath the spillet.

The next process addressed is spreading. This is done using the simple three regime mechanism proposed by FAY (1969). There is a slight modification to the Fay procedure in that the effective release time for a given spillet is a variable that can change during the evaluation of the spillet. This is described in the Appendix IV for subroutine SPREAD and is necessitated by the requirement that oil may be added to or removed from a spillet or its interfacial tension may be changed with time.

Oil is then evaporated from the spillet using the method developed by Wang, Yang and Hwang (1976). (See Appendix III subroutine EVAPOR 8). The Wang, et. al. formulation requires that the oil be divided into eight components, the fraction by weight of each component being supplied by the user. These fractions are given for several crude oils, a No. 2 fuel and Bunker C oil in Appendix IX.

Following the evaporation, the surface slicks are advected. This is done using the tidal currents plus (vectorially) 3.5 percent of the wind speed (see Subroutine SURDFT).

D. Subsurface Process

The subsurface processes (which are again called from one subroutine) are now performed (See Figure 6). The important feature of the subsurface portion of the model is the mixed Eulerian-Lagrangian coordinate system. The Eulerian coordinate system is the one on which the tidal currents, the bathymetry and the computational cells are defined. The Lagrangian coordinate system is the one on which the oil droplet concentration is defined and is parallel to and contained within the Eulerian bathymetry system. This system expands and translates so as to always include all particles. Variables defined on the Eulerian system are interpolated to the Lagrangian system. The Lagrangian system also allows for a coordinate transformation on z , the vertical variable, such that the water column at every horizontal node is divided into the same number of equally spaced layers. This means that as the water becomes shallower, the vertical grid spacing becomes smaller, thus keeping the same relative vertical resolution.

Prior to diffusing and advecting the marker particles in the water column, the Lagrangian system must be established. This is done by locating the extremes in x and y of the particle positions and then adding a buffer to these extremes. This defines the edges of the Lagrangian grid. The grid spacing is determined by dividing the distance between the edges of the grid by the number of grid elements. (see subroutine GRIDEX). This process is repeated each time step so that the droplets

SUBSURFACE

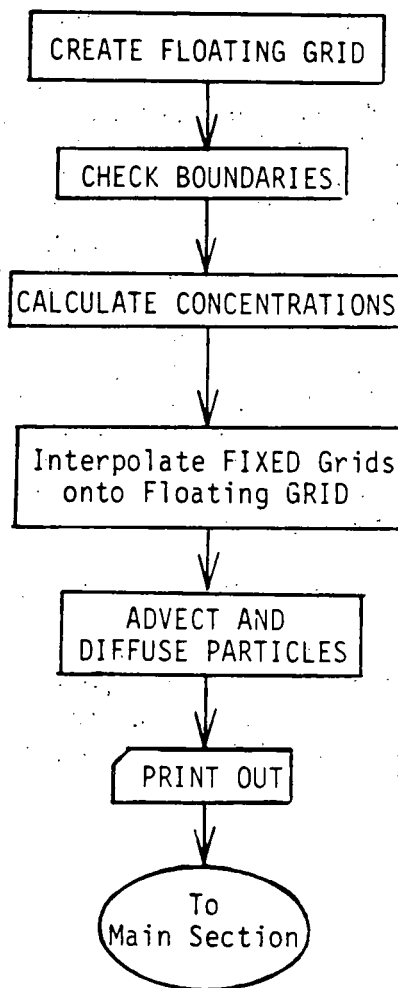


Figure 6. Flow Chart for Subsurface Portion of Simulation

never leave this grid. The program then checks the location of the droplets with respect to the computational cell grid (see subroutine BOUNV) and performs any necessary operations (e.g. deposits droplets on bottom or on shore). The concentrations are calculated at each of the floating grid locations (see subroutine CONC). Because the number of particles entrained in the first few time steps may be very small (say 100) and the concentration distribution calculated under such circumstances might be statistically unstable, this subroutine (CONC) is only called if a minimum number of particles (set by input parameter NCRIT) is exceeded. The next step is to interpolate the fixed grids values of tidal height, depth and currents onto the floating grid (see subroutine VELCT). Then, the diffusion velocities at each Lagrangian grid location are calculated and added to the advective terms. The particles are moved according to these velocities (see subroutine DISPV). The last step in the subsurface section is to output all requested subsurface information (see subroutine PRINT and output parameters KPRTU, KPRTC, KPRTP, NPRU, NPRC and NPRP in Appendix I). The output may go to paper and/or disk data sets, the latter being used as input to the plotting program. The step intervals for such output is controlled by a group of parameters input at the beginning of the run. The data output in PRINT are the concentration grid, the particle position array and the advective plus diffusive velocity Lagrangian grid. If the concentration was not calculated previously (i.e., if the number of particles is less than NCRIT), a new Lagrangian grid is created, the boundaries are checked and the concentration is calculated for printout. This terminates the subsurface portion of the simulation for the current time step.

E. Spill Overlap, Mass Balance and Restart Output

The next function of the main program is to add any spilllets which overlap by a certain percentage (Input parameter COMB) and also write the mass balance to paper and/or disk. The final step is to save the restart variables if this step is an even multiple of NSUMM, the output interval for the restart data set.

CHAPTER V REFORMATTING AND PLOTTING PROGRAMS

A series of programs capable of reformatting and plotting the results of a simulated spill have been written to accompany the oil spill model. The relationship between each of the programs in the output and the data output from the model is shown in Figure 7. There are three possible plotted outputs of data resulting from a simulation.

- i. Mass balance versus time (program PLOTMASS)
- ii. The areal extent of the subsurface oil exceeding a given concentration and the areal extent of the surface slick greater than a given thickness, both as a function of time (program PLOTAREA)
- iii. The spatial distribution of both subsurface and surface oil at a given instant in time (program PLOTMAP).

As indicated in Figure 7, the data output to disk by the simulation model is in the correct format for direct input to the mass balance plotting program. Both of the other plots, on the other hand, require at least one intermediate program to work the model output data into an appropriate form for input to the plotting routines. In particular, although the concentration distribution is output along with the other output parameters, it may be desirable to recalculate the concentration distribution on a grid different than the Lagrangian grid of the model. This is done by the program PARTICLE for those times in which sub-surface particle positions were output to disk. Prior to input into either PLOTAREA, PLOTMAP or CHECDATA, the concentration grid data, as well as the spill data, must be passed through the reformatting program DATAOUT. This step is executed after recalculation of the concentration grid (if performed) as indicated in Figure 7.

Once the data has been reformatted, it may be verified by the program CHECDATA or plotted by PLOTAREA or PLOTMAP.

Each of the programs outlined in Figure 7 are briefly described below. All plotting programs make use of a CALCOMP Plotter with standard Calcomp subroutine calls. The detailed descriptions of these programs are included in Appendix VI.

A. PLOTMASS

The flow chart for the program PLOTMASS is included in Figure 8. There are two sets of input to this program; mass data output by the simulation model and plot control parameters defined by the user. These are input as shown in Figure 8. As indicated in the Figure, the user may plot the output of several different simulations in one run of PLOTMASS, or s/he may plot several different mass balance plots for the same simulated spill. The plot control parameters specify, among other things, the various mass quantities (atmosphere, surface, etc.) to be plotted. Finally, the program allows the data from two separate simulations to be plotted on the same graph for comparison.

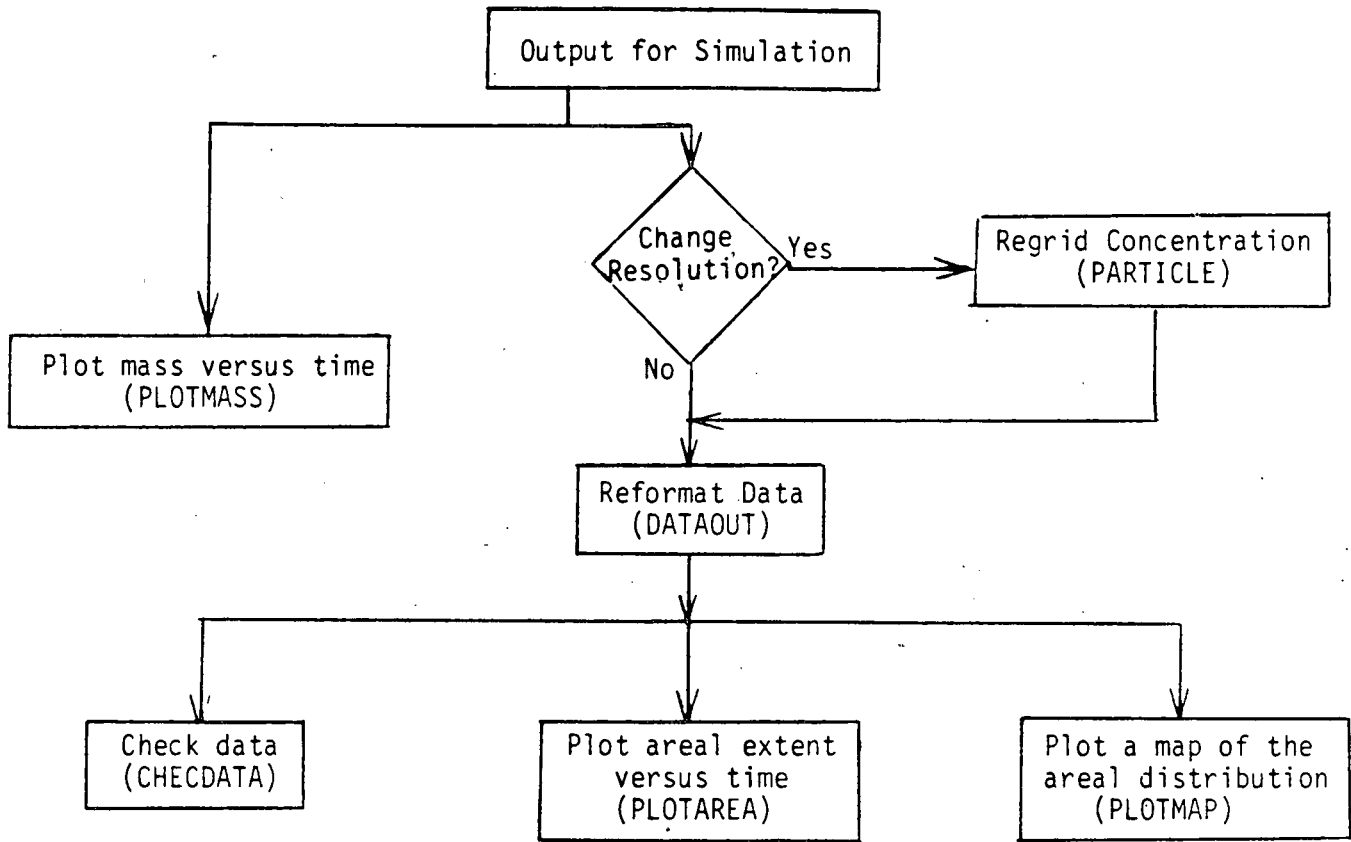


Figure 7. Overview of Output Program Sequence

PLOTMASS

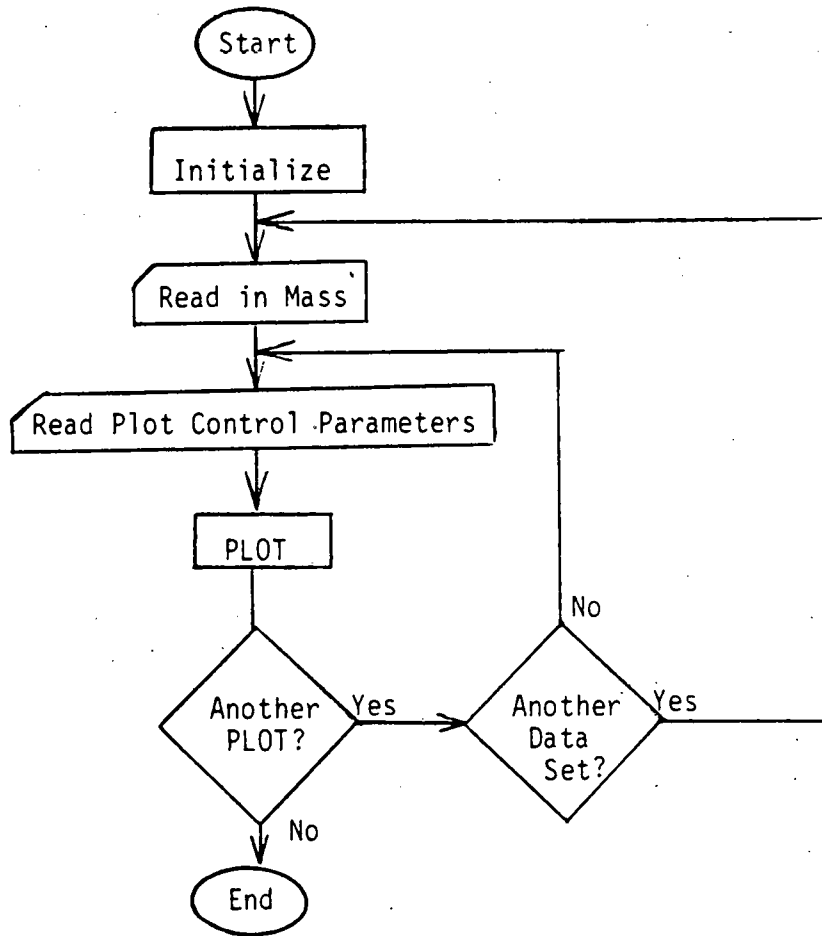


Figure 8. Flow Chart for Program PLOTMASS

B. PARTICLE

As indicated above, this program is used to calculate the concentration distribution on a grid different from the Lagrangian grid set up by the model. It requires, as input, the particle positions output by the simulation model, as well as those parameters required to define the new grid. The user supplies the latter. The flow chart for the program PARTICLE, is shown in Figure 9. The routines in this program that perform the required calculations have been extracted directly from the main program, hence, perform the calculations in exactly the same fashion.

C. DATAOUT

This program serves four functions. First, it compresses the data output by the oil spill model. Second, it integrates the surface and subsurface data sets into one data set for input to the plotting programs. Third, it performs cuts on both the surface distribution, by thickness, and on the subsurface distribution, by concentration. Fourth, it reads particle position data, (if requested) to be used by the program CHECDATA in verifying the output of the simulation. The overall operation of this program is outlined in the flow chart shown in Figure 10.

D. CHECDATA

This program simply reads the output of DATAOUT and prints it in an easy to read fashion for quick verification. The execution of this program is not required to plot the data.

E. PLOTAREA

The program PLOTAREA, see Figure 11 for its flow chart, is used to plot the areal extent of the surface and subsurface distribution. It reads the data output by DATAOUT from which the areal quantities are calculated. In the calculation for the area covered by the spillets, no attempt is made to account for the overlap of spillets, hence, the areal extent of surface oil will be overestimated if there is overlap. The user may elect to plot for one simulation only the surface and/or the subsurface. Or, s/he may elect to plot the output of two different simulations on the same plot for comparison.

F. PLOTMAP

The program, PLOTMAP, shown in the flow chart of Figure 12, allows the user to plot a map of the spill, showing both the surface and subsurface distribution of oil. Using the surface/subsurface data set output by DATAOUT. In addition, this program requires a set of control parameters that define the plots to be performed. There is a third optional input data set and that is the shoreline. The user may elect to plot the surface and/or the subsurface on a single plot at a given instant in time or s/he may elect to plot on a single plot these quantities at a number of different times. The user may also specify the times at which such plots are to be performed, as long as surface and/or sub-surface data was output by the main simulation at these times. The real use of this parameter is in limiting the plotting output in the case where, say maps for the 10, 20 and 30 day of a 30 day spill are desired, but the model

PARTICLE

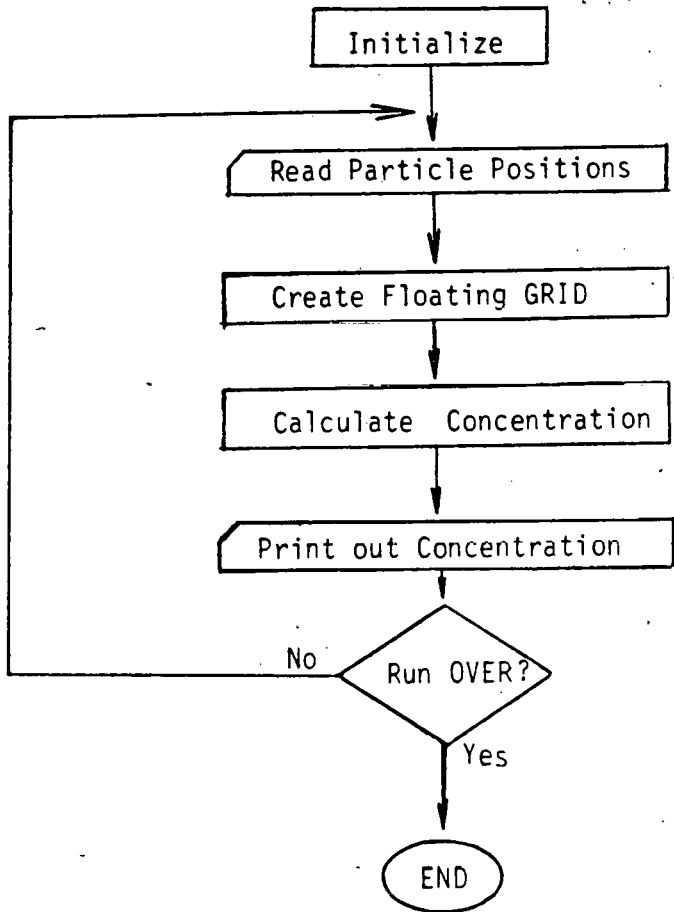
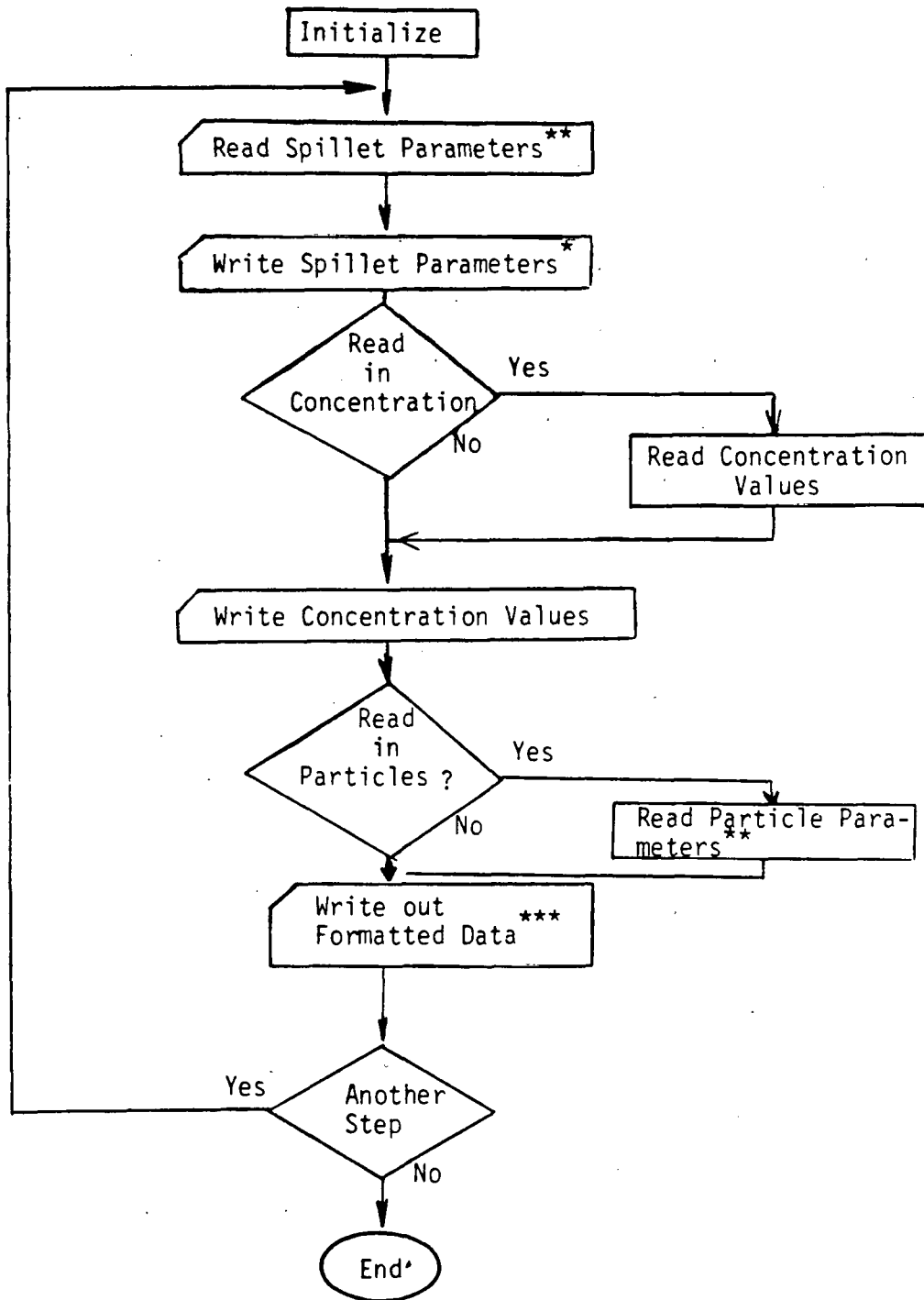


Figure 9. Flow Chart for Program PARTICLE

DATAOUT



NOTES: * write out for plotting data set if needed
** print out as read in
*** printout in formatted manner

Figure 10. Flow Chart for Program DATAOUT

PLOTAREA

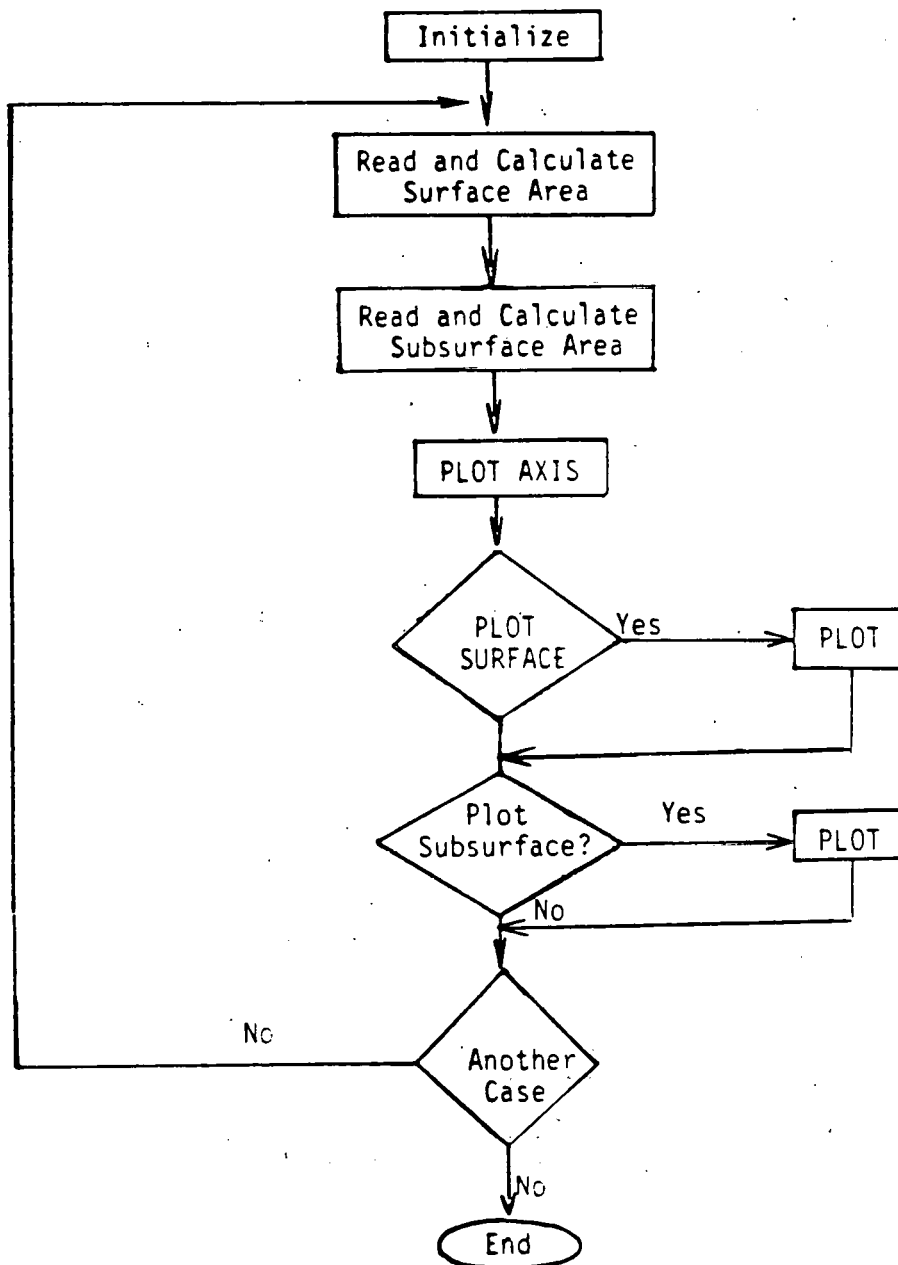


Figure 11. Flow Chart for Program PLOTAREA

PLOTMAP

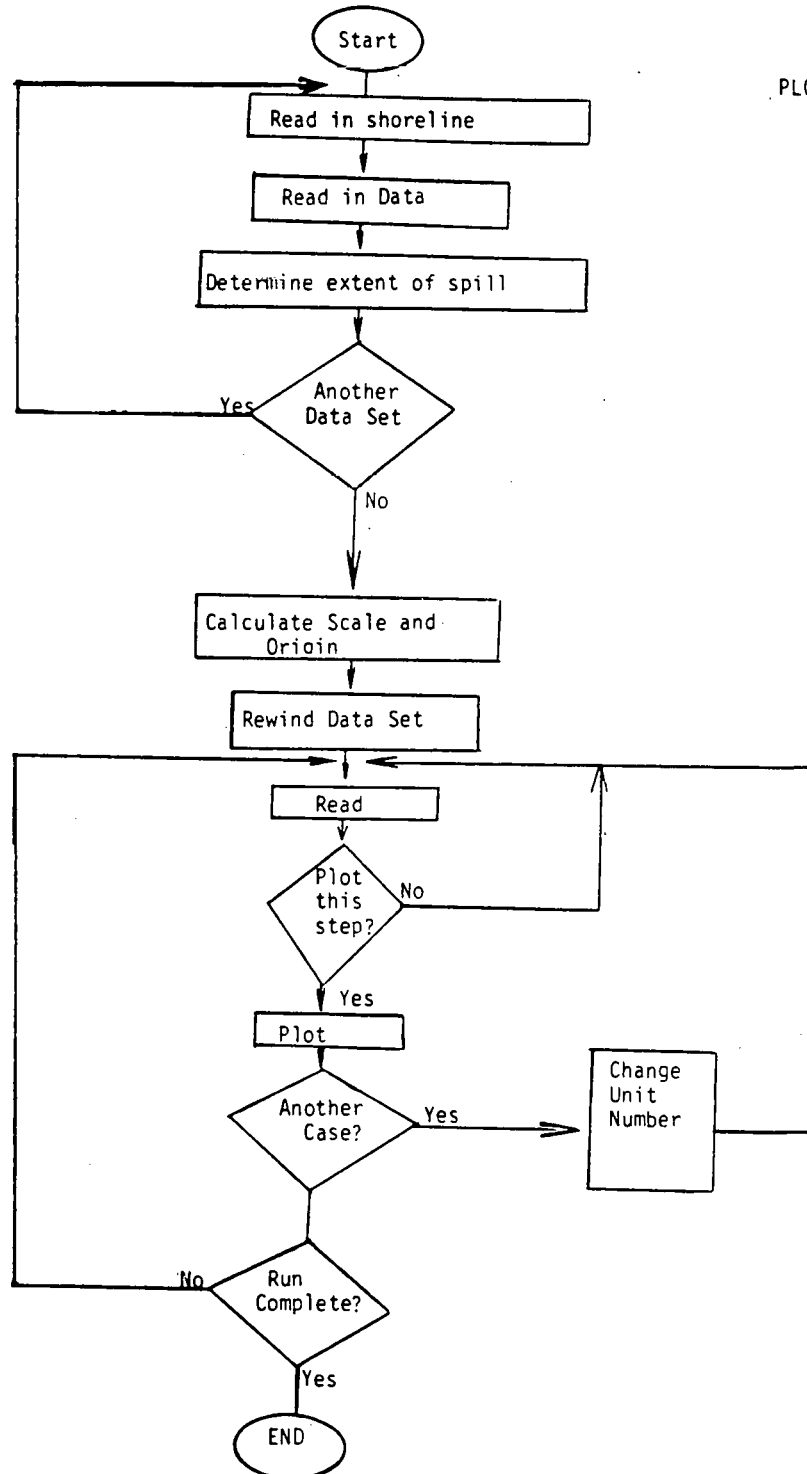


Figure 12. Flow Chart for Program PLOTMAP

outputs sufficient data to generate maps every day. Again, the user must remember that only the spilletts exceeding the thickness defined in DATAOUT and the region in which the concentration exceeds the level also defined in DATAOUT, will be plotted. To obtain maps of lower concentration values, DATAOUT must be rerun. As in the case of PLOTAREA and PLOTMASS, two simulation runs may be compared on one map.

APPENDIX I: Input Parameters and Formats for the Preview Run and the Main Simulation

A. Environmental Variables

Input Data Format

In Chapter II GRIDS, a program that will format environmental data for input to the main programs is described. For the user who elects not to use this program, the format structure of the environmental data is described here. First, the grid name and definition is input. Specifically, the variables NAM, VAR1, UNITS1, VAR2, and UNITS2 are read unformatted or with the format (13A4). See Table I-1 for a description of each variable. The name of the grid entered in NAM must be exactly as given in Table 3 (Chapter 2) and must be left justified. The next logical input record contains IMAX, JMAX, ANGLE, XL, YL, XS, YS, UNITS3, again either unformatted or with format:

(2I5, 3F10.6, 2F10.4, 2A4)

Finally the grid itself is read in. Again the option is either unformatted or formatted. In the unformatted case, the entire grid is read in as one logical record, the implied do loop on X (east to west) then on Y (south to north). If the grid contains two parameters, e.g., u and v, two logical records are required, one for each parameter. Some grids are real and some integer. (See Table 3, Chapter 2, for a definition of which are real and which are integer, as well as which are two parameters and which are only one). For the case in which the grid is real and is to be formatted, the format is:

(10F6.2)

Each row begins a new logical record and is read from left to right (west to east) starting at the lowest y or southernmost row of the grid and moving up. For two parameter arrays, first the entire array for one parameter is read and then the second parameter is read with exactly the same format.

For integer variables, the fashion in which the data is read is the same, only the format differs.

(15I4) replaces (10F6.2)

Table I-2 presents the read statements as they appear in ARAYIN.

B. Oilspill Variables

1. General Description

As discussed in Chapter I, spilled oil is represented in the simulation either as spilletts, circular puddles of oil on the surface, or droplets, representative droplets of oil in the water column. In its present configuration, only spilletts may be defined by the user. Droplets are either defined by the program or read in under the restart capability, but the user does not have easy access to this means of entering data.

TABLE I-1

Variable	Format	Description
NAM (3)	3A4	Name of input grid used for print-out. These must be exactly as written in Table III, Chapter I under Title.
VAR1(2)	2A4	Name of the first variable of the grid; used for printout.
UNITS1(3)	3A4	Dimensions of the first variable used for printout. (meter, degrees per/sec., etc.)
VAR2(2)	2A4	Name of second variable of the grid.
UNITS2(3)	3A4	Dimensions of the second variable.
IMAX	I5	Number of elements in the x direction.
JMAX	I5	Number of elements in the y direction.
ANGLE	F10.6	Angle measured from lines of constant latitude to the positive x-axis of the grid in the counter-clockwise direction (degrees).
XL, YL	F10.6, F10.6	Location of the (1,1) element of the grid (Longitude and Latitude).
XS, YS	F10.4, F10.4	Spacing between grid lines in x and y directions, respectively (meters or degrees, see input variable ISCAL).
UNITS3(2)	2A4	Dimensions of XS and YS.
ARRAY1	see Table IV	Values at grid nodes for first grid if real.
ARRAY2	see Table IV	Values at grid nodes to second variable if two grids describe one environmental variable.
MARRAY1	see Table IV	Values at grid nodes for first grid if integer.
MARRAY2	see Table IV	Values at grid nodes for second grid if required.

TABLE I-2 INPUT IN SUBROUTINE ARAYIN

Formatted

line number		
12		Read (ND,100) NAM, VAR1, UNITS1, VAR2, UNITS2
13	100	FORMAT (13A4)
14		READ (ND,105) IMAX, JMAX, ANGLE, XL, YL, XS, YS, UNITS3
15	105	FORMAT.(215, 3F10.6, 2F10.4, 2A4)

Unformatted

line number		
18		READ (ND) NAM, VAR1, UNITS1, VAR2, UNITS2
19		READ (ND) IMAX, JMAX, ANGLE, LX, YL, XS, YS, UNITS3
60-83	C	HERE TO READ UNFORMATTED REAL VARIABLES.
	C	
	40	CONTINUE
		READ (ND) ((ARRAY1 (I,J), I=1, IMAX), J=1, JMAX)
		IF (NO.EQ.1) GO TO 80
		READ (ND) ((ARRAY2 (I,J), I=1, IMAX), J=1, JMAX)
		GO TO 80
	C	
	C	HERE TO READ UNFORMATTED INTEGER VARIABLES.
	C	
	50	CONTINUE
		READ (ND) ((MARAY1 (I,J), I=1, IMAX), J=1, JMAX)
		IF (NO.EQ.1) GO TO 90
		READ (ND) ((MARAY2 (I,J), I=1, IMAX), J=1, JMAX)
		GO TO 90
	C	
	C	HERE TO READ FORMATTED REAL VARIABLES.
	C	
	60	CONTINUE
		DO 62 J=1, JMAX
		READ (ND,110) (ARRAY1 (I,J), I=1, IMAX)
	110	FORMAT (10F6.2)
	62	CONTINUE
		IF (NO.EQ.1) GO TO 80
		DO 64 J=1, JMAX
		READ (ND,110) (ARRAY2 (I-J), I=1, IMAX)
	64	CONTINUE
		GO TO 80
	C	
	C	HERE TO READ FORMATTED INTEGER VARIABLES
	C	
	70	CONTINUE
		DO 72 J=1, JMAX
		READ (ND,120) (MARAY1 (I,J), I=1, IMAX)
	120	FORMAT (15I4)
	72	CONTINUE
		IF (NO.EQ.1) GO TO 90
		DO 74 J=1, JMAX
		READ (ND,120) (MARAY2 (I,J), I=1, IMAX)
	74	CONTINUE

A spilllet is described by positional parameters, physical parameters, and chemical parameters (See Table I-3). The user is required to specify all parameters describing a spilllet for the time when it is first to appear.

It is not necessary that the spilllet be fresh in the sense that the oil has just escaped from a well, tanker, or pipeline. If the user would like to simulate a spill starting several weeks after the initial catastrophe, it suffices that s/he enter spilllets representing the locational, physical, and chemical variables as they are at that time. The model takes over from that point.

2. Input Data Format

Oil Spill parameters are entered in two logical records. The first record reads:

BSPIL, DSPIL, RSPIL, SSPIL, TSPIL, USPIL, WSPIL, XSPIL and YSPIL

with the format

(6F8.3, E8.2, 2F8.3)

The units assumed by the program are shown in the list of spilllet variable in Table I-3.

Following this the composition of the spilllet is input from one logical record containing between one and eight numbers each representing the fraction of a given hydrocarbon class.

The format of this record is:

(8F5.2)

The number of hydrocarbon classes is defined by the user through the parameter MSPIL discussed in the run control section. This variable is specified once per run, i.e., all spilllets are required to have the same number of hydrocarbon classes. The program, as currently configured, uses all eight classes. The fraction of each of the eight classes for four different types of oil, as well as a chemical description of each class, is given in Appendix IX. The user must exercise great caution if s/he decides to use a different set of hydrocarbon classes from the eight outlined in Appendix IX. In particular, the coefficient defining vapor pressure for each class included as data in the evaporation subroutine will have to be changed if the classes are restructured.

The format statements as they actually appear in the subroutine that reads in spilllet parameters are shown in Table I-4.

C. Treatment Variables

1. General Description

TABLE I-3
SPILLET PARAMETERS

Variable name	Description
BSPIL	Beginning time of spilllet (hours).
DSPIL	Density of oil (gm/cc).
RSPIL	Radius of spilllet (meters).
SSPIL	Interfacial tension of oil (dynes/cm).
TSPIL	Density of oil at time equal zero (gm/cc).
USPIL	Kinematic viscosity of oil (centistokes).
WSPIL	Weight of oil in spilllet (metric tons).
XSPIL	Longitude of center of spilllet.
YSPIL	Latitude of center of spilllet.
GSPIL	Mass fraction of each class of oil.

TABLE I-4

FORMAT OF SPILLET PARAMETER INPUT

```

100 1 READ (ND,100) BSPIL(I), DPSIL(I), RSPIL(I), SSPIL(I), TSPIL(I),
      USPIL(I), WSPIL(I), XSPIL(I), YSPIL(I)
      FORMAT (6F8.3, E8.2, 2F8.3)
      READ (ND,101) (GSPIL (I,J), J=1, MSPIL)
      FORMAT (8F5.2)

```

TABLE I-5
PHYSICAL CLEANUP PARAMETERS

Variable name	Description
BCLN	Beginning time of effort (hours).
DCLN	Duration of this effort (hours).
ECLN	Efficiency of effort.
RCLN	Radius of effort (meters).
VCLN	Volume rate of cleanup effort (metric tons/hour).
XCLN	Longitude of center of cleanup effort.
YCLN	Latitude of center of cleanup effort.

TABLE I-6
CHEMICAL TREATMENT PARAMETERS

Variable	Description
BCHEM	Beginning of this effort (hours).
DCHEM	Duration of this effort (hours).
PCHEM	Fraction of oil entrained.
RCHEM	Radius of this effort (hours).
SCHEM	Interfacial tension of treated oil (dynes/cm).
TCHEM	Toxicity of dispersant.
VCHEM	Volume rate of dispersant used (liters/hour).
WCHEM	Dispersant used per square meter (liters/meter ²).
XCHEM	Longitude of center of effort.

Available in this model are two response alternatives to the simulated spill. One alternative is the chemical dispersion of the spill and the other is the mechanical cleanup of the oil. Both methods may be used simultaneously and for each method there may be up to ten efforts in progress at once. The algorithm employed to implement a spill response effort is discussed in a later chapter. A response to the spill is not required for a simulation.

2. Input Data Format

All seven mechanical clean-up variables are read in one logical record in alphabetical order with the format:

(7F10.3)

The variables are listed in Table I-5 along with the units assumed by the program.

In the case of chemical treatment, there are ten variables. These are again read in alphabetical order, this time however, in two logical records. The format used for chemical treatment variables is:

(5F10.3)

These variables, along with the appropriate units, are listed in Table I-6.

The read statements and associated format for both the mechanical cleanup and chemical treatment variables are shown in Table I-7.

TABLE I-7 FORMAT STATEMENTS FOR RESPONSE VARIABLES

a. Mechanical Cleanup

```
READ (ND,100) BCLN (I), DCLN (I), ECLN (I), RCLN (I),  
1          VCLN (I), XCLN (I), YCLN (I)  
100 FORMAT (7F10.3)
```

b. Chemical Treatment

```
READ (ND,100) BCHEM (I), DCHEM (I), PCHEM (I), RCHEM (I), SCHEM (I),  
1  TCHEM (I), VCHEM (I), WCHEM (I), XCHEM (I), YCHEM (I)  
100 FORMAT 5F103
```


D. Run Control Variables

1. General Description

Run control variables include all parameters that control the evolution of a spill simulation but which, other than their association with the model, have little physical significance. All run control variables except the step control parameters are read in only once. A set of step control parameters is read in for each step. These parameters direct the model to read (or not to read) environmental variables, spill variables, and response variables for the given time step. In the first step, a grid must be read in for each environmental variable. In addition, at least one spill must be entered. All run control variables have been separated into three groups: general run control, subsurface control, and step control. These variables are listed in Table I-8 to I-10.

2. Data Input Formats

All run control variables except shoreline points and step control parameters are read in a similar format by one of the two subroutines READI and READF. READI is used to enter fixed point (integer) variables while READF is used for floating point (real) variables. They each require a logical record for each new variable entered. In addition, they require the name of the variable as used in the program. If an incorrect name is specified or the cards are out of order, a message is printed and the run terminated. In addition, integer variables must lie within a given range or the program will again print a message and the run will be terminated. These precautions are included to guard against an error associated with the input cards being out of order, a card forgotten or an integer variable entered one or more columns to the left of the desired location. The format for integer variables is:

(I15, 5X, A8)

where the A8 portion is to include the variable name left justified precisely as indicated in Tables I-8 and I-9. The format used for floating point (real) variables is:

(F15.5, 5X, A8)

where again A8 is the variable name.

Shoreline points are read in unformatted. Two logical records are required; one for x, longitude, and one for y, latitude. If NSHOR, the number of shoreline points, is zero, this read will be skipped.

All eight step control parameters are entered in one logical record in the following order:

NP, NV, NT, NK, NS, LSPIL, LCLN, LCHEM

These variables will be zero if no action is to be taken, one if the associated environmental grid is to be read in and equal to the number of

TABLE I-8 General Run Control Variables

Variable	Subroutine used	Range	Explanation
NSTRT	READI	0-1	0 - this run is not a restart 1 - this is a restart, the restart data set will be read.
NSTFN	READI	0-1	0 - this restart run uses new output data sets. 1 - this run uses previous output data set.
NSUMM	READI	0-100	Interval number of steps for writing out restart variables in the subroutine SUMMUP.
NRUN	READI	0-1	0 - total spill simulation. 1 - this activates the Preview run only (see Chapter III).
IDAY	READI	1-365	Day of year on which the spill begins.
NENV	READI	0-100	Print control parameter for formatted output of step control parameters in main program 0 - no printout 0 - prints out at this step interval.
DT	READF	1-2	Size of time step in hours.
TIMMAX	READF		Length of simulation (hours).
ISCAL	READI		1 - select small scale mode 2 - select large scale mode (see Chapter II).
NPRTA	READI	-1,0,1	Environmental grid printout control parameter (see Subroutine ARAYIN). -1 - no printout 0 - limited printout 1 - full printout
NPRTC	READI	0-1	Print control for cleanup and treatment efforts. 1 - printout all current cleanup and treatment efforts 0 - printout only newly started efforts.
NR	READI	1-20	Input file for step control parameters.
NCD	READI	1-20	Unit from which computational cell grid is to be read.

NCU	READI	1-4	Computational cell grid format control parameter. 2 - unformatted integer 4 - formatted integer
NDD	READI	1-20	Unit number from which the bathmetric grid is to be read.
NDU	READI	1-4	Bathmetric grid format control 1 - unformatted real 3 - formatted real
NED	READI	1-20	Unit number from which the tidal elevation grid is to be read.
NEU	READI	1-4	Tidal elevation grid format control (See NDU).
NKD	READI	1-20	Unit number from which the temperature grid is to be read.
NKU	READI	1-4	Temperature grid format control (see NDU).
NSD	READI	1-20	Unit from which sea state grid is to be read.
NSU	READI	1-4	Sea state grid format control (see NDU).
NTDU	READI	1-20	Unit from which the U components (x-direction) of current are to be read.
NTDV	READI	1-20	Unit from which the V components (y-direction) of current are to be read.
NTUU	READI	1-4	Format control for x current grid. (See NDU).
NTUV	READI	1-4	Format control for y current grid.
NWD	READI	1-20	Unit number from which the wind grid is to be read.
NWU	READI	1-4	Wind grid format control (see NDU).
NCHD	READI	1-20	Unit number from which the chemical treatment data is to be read in.
NCLD	READI	1-20	Unit number from which the physical cleanup data is to be read.
NSHD	READI	1-20	Unit number from which the shoreline points are to be read.
NSPD	READI	1-20	Unit number from which new spilllet information is to be read.
NMAX	READI	1-2100	Maximum number of droplets allowed. This parameter is used to dynamically allocate

NTCLASS	READI	1-200	space for x,y,z and NORDR in the subsurface subroutines. These variables are currently dimensioned of 2100 in the main program. Maximum number of particle classes allowed. The dimensions will allow 200 different types of particles.
NUMCL	READI	1-200	Maximum number of particles per class.
XMSPAR	READF		Amount of oil to be represented by each droplet metric (tons).
MAXSPL	READI	1-99	Maximum number of spilletts allowed. Dimension statements currently limit this to 100.
COMB	READF		Percentage of overlap needed in order to combine two spilletts (see Subroutine ADD).
MSPIL	READI	1-9	Number of components of oil. Due to the evaporation model, this is how set at 8.
NSPPRO	READI	-1-100	Spillet print control parameter for disk data sets. This gives the interval (in steps) of how often to write out spillet information. (see Subroutine SPILIN).
NSPPRP	READI	-1-100	Spillet printout control parameter. -1 - no printout 0 - printout only on first step 0 - printout interval
NSHOR	READI	0-1500	Number of shoreline points.

TABLE I-9 SUBSURFACE CONTROL VARIABLES

Variables	Subroutine used	Range of Values	Explanation
POWX	READF		Power of length factor in scale dependent diffusion equation in x-direction (see Subroutine DIFF).
POWY	READF		Power of length factor in scale dependent diffusion equation in y-direction (see Subroutine DIFF).
EXX	READF		Coefficients used in scale dependent diffusion equation for the x direction.
EYY	READF		Coefficient used in the scale dependent diffusion equation for the y direction.
NTRANS	READI	0-1	Parameter for vertical transformation. 0 - uses depths as read in. 1 - normalizes all vertical distances by the depth.
DXX, DYY, DZZ	READI		Constant diffusion coefficients in the x, for Lagrangian Coordinate System. Same y Same z
DYY DZZ NSUB	READI	0-1	Control parameter for analytical diffusion. 0 - do not use 1 - use analytical sub-grid diffusion until standard deviation of cloud is comparable to grid mesh.
NDIFF	READI	0-1	Control parameter for using scale dependent diffusion. 0 - use constant coefficients 1 - calculate scale dependent diffusion equations (see Subroutine DIFF).
NCRIT	READI	0-1000	Minimum number of particles needed to calculate concentration for use in diffusion.
NEXTR	READI	0-1	Control parameter for Lagrangian grid. 0 - use fixed grid 1 - use Lagrangian grid

DEPC	READF		Vertical origin of initial particle distribution (meters)
POMIN	READF		Gives the minimum spacing in meters in the x and y-directions if only two particles are present. If the particles are too close together, the Lagrangian grid cannot be created around them without having an error.
AFRAC	READF		Determines the fraction of particles within RO (RO is radius of spillet divided by RIFRAC, see Subroutine ENTRN and INJECT).
RIFRAC	READF		Radius up to which particle density is uniform (see Subroutines ENTRN and INJECT).
HENT	READF		Length of time of entrainment for use in calculating the maximum radius of the initial particle distribution (see Subroutine ENTRN).
DDIAMT	READF		Diameter of droplets (mm).
DVELZT	READF		Vertical velocity of droplet (m/sec). Zero if neutrally buoyant.
NPTSUB	READI	-1 -1	Controls printout of subsurface information concerning Lagrangian grid (Subroutine GRIDEX) and scale dependent diffusion (Subroutine DIFF). -1 - no printout 0 - print only on first step >0 - printout at this step interval.
NPRTMS	READI	0-100	Print control parameter for mass balance. This is given in an interval number of steps and controls paper and disk printout.
KPRTV	READI	0-100	Print control parameter for formatted paper output of Lagrangian grid velocity values, concentration values and particle parameters respectively. This is given in an interval number of steps.

NPRD	READI	0-1	Control parameter for indicating that some disk data set output is requested. 0 - no output 1 - if any printout of concentration or particle parameters is desired.
NPRU, NPRC, NPRP	READI	0-100	Interval control in number of steps for printout of velocity, concentration or particle disk data sets.
NUSP	READI	1-20	Spillet output unit number.
NUPS	READI	1-20	Restart data output number.
NUCN	READI	1-20	Concentration unit number.
NUPT	READI	1-20	Particle parameter unit number.
NULV	READI	1-20	Velocities Lagrangian unit number.
NUMS	READI	1-20	Mass unit number.
NUDP	READI	1-20	Deposited particle unit number.
NULT	READI	1-20	Lost particle unit numbers.

spilletts, cleanup efforts, or treatment efforts to be read in. The format used is:

(8I5)

NOTE: One logical record with these eight parameters is read in for each time step of the model. The variables and their definition are shown in Table I-10.

E. Restart Variables

Restart variables are all the parameters required to restart a simulation which may have been terminated for one of three reasons: (1) program or system error that resulted in an abnormal termination of a job, (2) the user, after having run a simulation for some predetermined number of time steps, and having examined the resulting output decides to extend the run, or (3) the user wishes to run the model at several different time steps and spatial resolutions, e.g., high temporal and spatial resolution followed by coarser resolution. All the parameters required to restart the model are written to disk (or tape) every NSUMM time steps (NSUMM determined by the user). The model may be restarted only at the time step following the last time step for which restart data were written.

When a run is to be restarted, the run control variable NSTRT is set equal to 1. If the run is to restart an abnormally terminated one, all data sets used in the previous run must be included. The model will read these data sets to the point where the previous run terminated. If the user specifies NSTFN = 0, the program only reads the restart data set and uses new input and output data sets. In addition, a number of variables generated by the simulation and output to the restart data set are read.

F. Input Sequence for all Input Data

Because the user may elect to read some of the environmental variables, treatment data, or spillet data from Unit 5 (the card reader, normally used for run control parameters), it is essential that the order in which all input data (except RESTRT) be known. This order is indicated schematically in Table I-II.

TABLE I-10 STEP CONTROL VARIABLES

Variable name	Description
NP	Wind grid control parameter.
NV	Tidal currents grid control parameter.
NT	Tidal heights grid control parameter.
NK	Temperature grid control parameter.
NS	Sea state grid control parameter.
LSPIL	Number of new spilletts this step.
LCLN	Number of new cleanup efforts this step.
LCHEM	Number of new treatment efforts this step.

Table I-11

INPUT LIST (in order of entrance, read down from left to right)

NSTRT	POWX	BATHMETRY GRID
NSTFN	POWY	
NSUMM	EXX	
NRUN	EYY	
IDAY	NTRANS	COMPUTATION CELL GRID
NENV	DXX	
DT	DYY	
TIMMAX	DZZ	
ISCAL	DX	The following are repeated each step if needed:
NPRTA	DY	
NPRTC	DZ	
NR	IMSUB	
NCD	JMSUB	STEP CONTROL PARAMETERS
NDU	KMSUB	
NDD	NSUB	WIND VELOCITY GRID
NDU	NDIFF	
NED	NCRIT	TEMPERATURE GRID
NEU	NEXTR	
NKD	DEPC	SEA STATE GRID
NKU	POMIN	
NSD	AFRAC	X - DIRECTION TIDAL CURRENT GRID
NSU	RIFRAC	
NTDU	ROFRAC	Y - DIRECTION TIDAL CURRENT GRID
NTDV	HENT	
NTUU	DDAMT	TIDAL LEVEL GRID
NTUV	DVELZT	
NWD	NPTSUB	
NWU	NPRTMS	
NCHD	KRPTU	
NCLD	KPRTC	PHYSICAL CLEANUP EFFORTS
NSHD	KPRTP	
NSPD	NPRD	
NMAX	NPRV	CHEMICAL TREATMENT EFFORTS
NUCLAS	NPRC	
NUMCL	NPRP	INITIAL SPILLET PROPERTIES
XMSPAR		
MAXSPL		
COMB	READ THRU	
MSPIL	RESTART SECTION	
NSPPRD		
NSPPRP		
NUSP		
NURS		
NUCN		
NUPT		
NUVL		
NUMS		
NUDP		
NULT		
NSHOR		
SHORELINE POINTS		

APPENDIX II: SIMULATION MODEL OUTPUT

The output from the simulation model takes one of two forms; paper copy to allow the user to monitor a simulation, or digitally stored data (either on disk or tape) to be used as input to the plotting programs (See Fig. II-1). Because the model is capable of generating enormous volumes of data in both cases, a number of printout parameters have been added to the model. In general, output to paper is treated by a different set of parameter than that to disk or tape allowing for the two different modes to be treated separately.

A. Printed output used to monitor a run (Generally UNIT 5)

First, all of the input parameters read by either READI or READF are written out as they are read. There is no choice in the output of these parameters. For the remaining input parameters, environmental grids, response alternatives, and spillet characteristics the user does have a choice of the amount of output.

Every timestep, the program reads in a set of parameters which control that step. This command list may be printed out if desired under the control of the parameter NENV. If NENV is zero, no printout is generated. For NENV greater than zero, the step control information is printed every NENV step.

The output of all environmental grids is controlled by one parameter NPRTA. Any environmental input data written out will start on a new page so the user must therefore take great care here when selecting environmental output for a long simulation. For example, a 30 day simulation with three hour timesteps and a new current grid and wind grid each timestep will require at least 480 pages to print out just these two data sets. To suppress environmental grid output set NPRTA=-1. Limited printout defining the grid location and orientation only is selected with NPRTA=0. The entire grid is printed out with NPRTA=1.

Mechanical cleanup and chemical treatment efforts may also be summarized on paper. The controlling parameter for this output is NPRTC: its value being 0 when only new efforts are to be printed out and 1 when all current efforts are to be printed out. If NPRTC equals 1, this information is printed out for every timestep for which there exists a response effort, new or ongoing.

The spillet printout control variable is NSPPRD and is used to define the interval at which the defining variables for each spillet are printed out. NSPPRD=-1 suppresses all output while NSPPRD=0 prints out only on the first timestep (at which time at least one spillet must be released). If NSPPRD is greater than zero, then spillet information is printed out for the first step, the last step, and at any other step number that is a multiple of NSPPRD; eg. NSPPRD=3 would result in all spillet information being printed on the 1st, 3rd, 6th, 9th, ..., last steps. Again, caution must be exercised when specifying this parameter as the output can become voluminous; eg. if the run has 39 spillets and runs for 30 days and the spillet data is printed out every timestep, approximately 2000 pages of output would be generated (12 lines/spillet * 39 spillet, = 8 pages/timestep x 240 timesteps=1920 pages).

Summary Order of Output II-1

D - Disk Data Sets

P - Paper

(all controlled by parameters)

ALL OUTPUT CONCERNED WITH INPUT	P
FLOATING GRID DEFINITION	P
SCALE-DEPENDENT DIFFUSION	P
CURRENT VELOCITIES	P, D
FLOATING GRID DEFINITION	P
CONCENTRATION PARAMETERS	P, D
PARTICLE PROPERTIES	P, D
VELOCITY VALUES	P, D
MASS BALANCE	P, D
RESTART PARAMETERS	D

In addition to the input parameters described above, there are three other groups of data that may be output to the printer. The first such group consists of two separate pieces of information specifically, the subsurface grid definition variables and the subsurface diffusion parameters. The grid definition variables locate the Lagrangian grid and define the size of the associated grid elements. The subsurface diffusion variables consist not only of the values of the scale dependent diffusion, but also of the statistical characteristics of the cloud of entrained particles used to obtain the scale dependent diffusion. The printout of all of the variables in this group is controlled by one parameter, NPTSUB. As in the case of spillet data, NPTSUB equal to -1 suppresses such printout, NPTSUB equal to 0 prints out only on the first step and NPTSUB greater than 0 prints out on steps that are multiple of NPTSUB and on the first and last steps.

The second group of derived variables, the printout which the user may control, defines the mass balance; e.g., mass evaporated, mass on the surface, mass entrained, etc., the controlling parameters in this case is NPRTMS. Not only does this parameter control printout to paper, but also to disk/tape; i.e., whenever data is written to the printer it is also written to the mass balance disk data set. This is an important set of parameters and takes little space either on disk or paper, hence, should in general be output fairly often. NPRTMS is greater than or equal to zero, printing out nothing when equal to zero, and every NPRTMS step otherwise.

The last group of derived data output are the particle locations and the velocity vectors and concentration values on the Lagrangian. Each of these is controlled by its own parameters, KPRTU, KPRTC respectively. All of these variables operate in the same fashion printing out nothing when equal to zero and printing out every KPRT (i) steps otherwise.

Finally, the program will print to paper warning or error messages when appropriate. The user has no control over the printout of such data.

All of the print control parameters for output to Unit 5 are listed with their meaning in Figure II-2.

B. Disk/tape output data sets.

There are seven possible output data sets; data sets written to disk or tape that can be used by other programs either to plot the results or to restart the simulation model as described in Chapter IV. These are summarized in Table II-2 and described in some detail below.

1. Restart

As described earlier, this data set contains all of the run generated variables needed to restart a run. Of course, all input data sets are also required, i.e., environmental variables, etc. The controlling parameter for this output is NSUMM, the restart data being written every NSUMM timesteps in addition to the last timestep if the previous run terminated with no errors. All restart data is written to Unit # NURS in the subroutine SUMMUP. Because a large volume of data is generally

Figure II-2

Control Parameter	Meaning (for more detailed information, see Figure I-8)
NENV	Step control printout environmental header
NPRTA	Controls printout of enviromental header
NPRTC	Controls printout of cleanup efforts, treatment efforts and spillet information
NSPPRP	Step control for spillet data
NPTFLT	Step control for subsurface information
NPTSUB	(see Subroutine SUBSUR)
KPRTV	Print control for floating grid velocity values
KPRTC	Print control for concentration values
KPRTP	Print control for particle parameters
KPRTMS	Print control for mass balance output

TABLE II-2
DISK DATA SETS

Data Set	Subroutine	Unit Number	Control Parameter	Memory Space Needed
Restart	SUMMUP	NURS	NSUMM	932 bytes plus 84 bytes per spillet and 16 bytes per particle.
Spillet	SPILIN	NUSP	SNPPRD	72 bytes per spillet.
Concentration	PRINT	NUCN	NPRC	80 bytes plus 4 times (number of X grid elements plus number of Y grid elements) plus (the number of X grid elements times the number of Y grid elements).
Particles	PRINT	NUPT	NRPD	80 bytes plus 4 times (the number of Y grid elements plus the number of Y grid elements (plus 56 times the number of classes plus 18 times the number of particles).
Mass	MASSC	NUMS	NPRTMS	36 bytes per step.
Lost Particles	BOUNV	NULT		32 bytes per particle.
Deposited Particles	BOUNV	NUDP		32 bytes per particle.
Velocity Components	PRINT	NUVL	NRDV	88 bytes times maximum number of X or Y grid elements.

output for every NSUMM timesteps, the decision was made to overwrite the previous restart data so that restart data exists only for the most recent multiple of NSUMM steps or if the previous run terminated successfully for the last step. This means that a run may only be restarted for the last timestep that restart data was written.

The space requirements for a restart data set depend both on the number of particles and the number of spilletts, the appropriate equation being

Space in bytes = $932 + 84 * (\text{Number of spilletts}) + 16 * (\text{Number of particles})$

The longest logical record is 88 bytes and the output data is unformatted (binary). The DD statement for the restart data set on an IBM 370 system with 39 spilletts and 2000 particles is:

```
FT01FO01 DD DSNAME = RESTART.DATA,  
          DISP = (NEW, CATLG),  
          UNIT = SYSDA,  
          DCB = (RECFM = VBS, LRECL = 88, BLKSIZE = 4404),  
          SPACE = (TRK, (40,10), RLSE)
```

Note: i. To save memory, it helps to single buffer all of the output data sets, i.e., set BUFNO=1 in the DCB parameter.

ii. 4 bytes have been added to the longest logical record because the data set is unformatted and 4 bytes have been added to each block for the same reason.

2. Spilletts

All spillet information is output every NSPPRP step to unit # NUSP by the subroutine SPILIN. This output is suppressed for NSPPRP=0. Because a time history of each spillet is desired for input to the plotting program, every NSPPRP step is appended to the data already written i.e., the space requirements of this data set grow with the length of the run and with an increased frequency of output. If a run is restarted, these data sets are read to the appropriate step and subsequent output is added to the end.

The data defining each spillet at a given timestep is output as one logical record 72 bytes in length. The DD statement for a 30 day run with spillet data output once per day and a total of 39 spilletts is:

```
FT FO01 DD DSNAME = SPILLET. DATA,  
          DISP = (NEW, CATLG),  
          UNIT = SYSDA,  
          DCB = (RECFM = VBS, LRECL = 76, BLKSIZE = 7604),  
          SPACE = (7604,(12,1),RLSE)
```

Note: Again, the data is output in binary, and DISP= OLD for a restarted run.

3. Concentration

The concentration grid is output in the subsurface subroutine PRINT and is controlled by the step parameter NPRC. It is written to unit # NUCN.

Each grid is output as three logical records; one locating the x grid nodes in the fixed depth grid, the second locating the y grid nodes, and the third giving the concentration at each node. The longest logical record is therefore a function of the number of x, y and z grid elements. For a 15*15*3 (x*y*z) grid, one concentration grid output per day for a 30 day run; the DD statement would take the form:

```
FT F001 DD DSNAME = CONC.DATA,  
        DISP = (NEW, CATLG),  
        UNIT = SYSDA,  
        DCB = (RECFM = VBS,LRECL = 2704, BLKSIZE = 8116),  
        SPACE = (8116,(10.1),RLSE)
```

Note: Again, the data is output in binary, and DISP = OLD for a restarted run.

4. Particles

The position of all particles currently in the water column will be output to unit # every NPRP steps by the subroutine PRINT. Because the particle positions are referenced to the lagrangian grid, the location of these grid elements is also output. Finally, the particle class information must be output. The total space requirements per time step are:

Space in bytes = $80+4*(\# \text{ of } x \text{ grid nodes} + \# \text{ of } y \text{ grid nodes}) + 56*(\# \text{ of particle classes}) + 18*(\# \text{ of particles})$

For a 15*15 (x*y) grid, with all particle information output once per day a 30 day run, 200 particle classes and 2000 particles, the DD statement would take the form:

```
FT F001 DD DSNAME = PART.DATA,  
        DISP = (NEW, CATLG),  
        UNIT = SYSDA,  
        DCB = (RECFM = VBS,LRECL = 68,BLKSIZE = 1296),  
        SPACE = (TRK, (100,50), RLSE)
```

Note: This data set can consume a large volume on the disk.

5. Mass Balance

The mass of oil in the various environmental categories dealt with in the model, water surface, water column, shore, etc., is output in the subroutine MASSC to unit #NUMS every NPRTMS timesteps. As in all previous cases, if the step control parameter is zero, no output is generated. A single logical record 36 bytes long is output every NPRTMS steps. For a 30 day simulation with two outputs per day, the DD statement would assume the form:

```
FT F001 DD DSNAME = MASS.DATA,  
      DISP = (NEW,CATLG),  
      UNIT = SYSDA,  
      DCB = (RECFM = VBS,LRECL = 40,BLKSIZE = 404),  
      SPACE = (404,(3,1),RLSE)
```

6. Lost Particles

Every time a marker particle passes out of the study area, all of its parameters as well as its location is written to unit #NULT. This is done in the subroutine BOUNV and is not under the control of the user. If this output is not desired, a dummy data set is required:

```
FT F001 DD DUMMY
```

If the output is desired, each particle lost to an open boundary will use 32 bytes hence the DD statement will take the form:

```
FT F001 DD DSNAME = LOST.DATA,  
      DISP = (NEW,CATLG),  
      UNIT = SYSDA,  
      DCB = (RECFM = VBS,LRECL = 36,BLKSIZE = 364),  
      SPACE = (364,(30,10),RLSE)
```

Note: In this case, the exact volume on disk required is not known because the number of particles lost is not known. Some upper limit must be estimated.

7. Deposited Particles

Because the user may desire a plot of the distribution of oil on the sea floor following a simulated spill, the characteristics and locations of each deposited particle are output to disk, unit #NUDP. All comments relevant to deposited particles are identical to those for lost particles and therefore are not repeated here.

8. Velocity Components

The floating grid velocity components are written to unit #NUVL in subroutine PRINT. The DD statement for a 15*15 grid will be:

```
FT F001 DD DSNAME = VEL.COMP,  
      DISP = (NEW,CATLOG),  
      UNIT = SYSDA,  
      DCB = (RECFM = VBS,LRECL = 88,BLKSIZE = 1588),  
      SPACE = (TRK,(90,10),RLSE)
```

This writes all 3 components so that much output is generated.

APPENDIX III: Variables in Common in the Main Simulation Program

In this Appendix, the variables in all of the common statements in the main simulation model are described. The descriptions are arranged in alphabetical order by common name. In addition to a description of the variable, the associated units are also defined.

- (1) /CHEM/ - defines chemical treatment
- LCHEM - number of new treatment efforts during this step.
 - NCHEM - total number of current treatment efforts.
 - NCHD - unit from which the treatment data shall be read.
 - BCHEM(ICHEM+)- 10*- time this treatment effort begins (hours).
 - DCHEM(ICHEM) - 10 - duration of treatment effort (hours).
 - RCHEM(ICHEM) - 10 - radius of treated area (meters).
 - SCHEM(ICHEM) - 10 - interfacial tension of treated oil (dynes/cm).
 - TCHEM(ICHEM) - 10 - unused.
 - VCHEM(ICHEM) - 10 - volume of dispersant used (liters/hour).
 - WCHEM(ICHEM) - 10 - dispersant used per square meter (liters/meter**2).
 - XCHEM(ICHEM) - 10 - center of treated area (Longitude).
 - YCHEM(ICHEM) - 10 - center of treated area (Latitude).
 - PCHEM(ICHEM) - 10 - percentage of oil entrained if treated area is larger than spilled area.
- (2) /CLEN/ - defines the physical cleanup effort.
- LCLN - number of new cleanup efforts during this step.
 - NCLN - total number of current cleanup efforts.
 - NCLD - unit from which the cleanup data shall be read.
 - BCLN(ICLN) - 10 - time this cleanup effort begins (hours).
 - DCLN(ICLN) - 10 - duration of this cleanup effort (hours).
 - ECLN(ICLN) - 10 - efficiency of this cleanup effort (%).
 - RCLN(ICLN) - 10 - radius of this cleanup effort (meters).
 - VCLN(ICLN) - 10 - oil recovery rate (tons/hour).
 - XCLN(ICLN) - 10 - center of this effort (Longitude).
 - YCLN(ICLN) - 10 - center of this effort (Latitude).
- (3) /CNTL/ -control parameters
- IMSUB, JMSUB, KMSUB - number of grid elements in the X, Y, and Z directions for Lagrangian Coordinate System (See description of subroutine GRIDEX for a better explanation).
 - NPRTA - printout control parameter for the environmental data (used in Subroutine ARAYIN).

*This numerical value indicates the size of the array as currently configured.

+ICHEM indicates that this parameter applies for each of the ICHEM treatment efforts of the NCHEM current efforts.

- 1 no printout
 - 0 limited printout
 - 1 full printout
 - NPRTC - printout control for cleanup and treatment efforts.
 - 1 printout all current cleanup and treatment efforts for every timestep.
 - 0 printout only when new efforts are started.
 - DT - timestep size (hours).
 - TIME - in seconds.
 - TIMMAX - time since start of spill at which run is to end.
 - ISCAL - 1 program does necessary distance calculations in meters.
 - 2 program does necessary distance calculations in degrees of Longitude or Latitude.
 - NSAV(99) - spilletts which have been removed in Subroutine ADD and added to the end of the spillet list.
- (4) /COMP/ - defines the computational cell as explained in Chapter II.
MAXCX, MAXCY - number of grid elements in X and Y.
AC - angle between the X axis and lines of constant Latitude (degrees).
MCOMP(MAXCX,MAXCY) -30,15 - computational cell definition.
XCL,YCL - Longitude and Latitude of the (1,1) grid position.
XCS,YCS - grid spacing in X and Y (meters or degrees).
- (5) /DENS/ - Den (8) - densities of the eight fractions of oil. These are initialized in the main program and listed in the section which describes the evaporation subroutine; EVPOR8. Sample values are given in Appendix IX.
- (6) /DEPOS/ NLOST - number of subsurface particles lost through a computational boundary.
NDEP - number of subsurface particles deposited on bottom.
- (7) /DIFU/ NCRIT - minimum number of particles needed before diffusion velocities are calculated. The time at which NCRIT is exceeded depends upon how fast the particles are being entrained.
NDIFF - control parameter for calculating scale dependent diffusion coefficients.
 - 0 use constant coefficients which are input.
 - 1 call subroutine DIFF which calculates scale dependent diffusion coefficients.
DXX,DYY,DZZ - diffusion coefficients in X,Y, and Z directions respectively (meters²/sec).
EXX,EYY - coefficient used in scale dependent diffusion equation.
POWX,POWY - power of length factor used in scale dependent diffusion equation.

- (8) /DPTH/ - fixed depth grid. The subsurface particles positions are tracked with respect to the origin of this grid.
MAXDX,MAXDY - number of grid elements in the X and Y directions.
AD - angle between X axis and lines of constant Latitude (degrees).
HGHT(MAXEX, MAXEY) - 30,15- depth of water at mean low tide (meters).
XDL,YDL - Longitude and Latitude of the (1,1) grid position.
XDS,YDS - grid spacing in the X and Y directions (meters or degrees).
- (9) /ELVN/ - tidal heights grid. Used in performing the Z coordinate transformation for the subsurface diffusion/advection calculation.
MAXEX,MAXEY - number of grid elements in the X and Y directions.
AE - angle between X axis and line of constant Latitude (degrees).
HGHT(MAXEX,MAXEY) -30,15- elevation of sea level due to tide (meters).
XEL,YEL - Longitude and Latitude of the (1,1) grid position.
XES,YES - grid spacing in the X and Y directions (meters or degrees).
- (10) /FLOT/ - velocity at floating grid nodes.
UFLT,VFLT,WFLT(IMSUB,JMSUB,KMSUB) (15,15,10) - advective current plus diffusion velocities at each of the floating Lagrangian Coordinate System grid nodes. (m/sec. or degrees/sec.)
- (11) /INJC/- passes definitions of the initial particle positions during entrainment and treatment. This is explained in detail in Subroutine ENTRN.
DEPC - verticle origin of initial particle distribution (meters).
AFRAC - determines the fraction of particles within RO (RO = RSPIL/RIFRAC).
RIFRAC - determines radius over which particle density is uniform (meters).
ROFRAC - factor which determines rate at which particle distribution falls off.
DDIAMT - diameter of entrained droplet (mm).
DDVELZT - z velocity of droplet, zero if neutrally buoyant.
HENT - length of time of entrainment for use in calculation of RMAX in Subroutine ENTRN (hours).
- (12) /MASS/- defines location of all mass for mass balance (all in metric tons).
XMATM - mass in atmosphere.
XMBIO - mass biologically consumed.
XMBOT - mass deposited on bottom.
XMCLN - mass physically cleaned up.

XMDMP - total amount of mass dumped up to that step.
XMLLOS - mass lost through boundaries.
XMSHP - mass deposited on shore.
XMSUR - mass left on surface.
XMSUS - mass in water column.

(13) /MAXVEL/ - passes maximum velocity for the courant number which is:
maximum velocity*timestep/grid spacing.
UAMAX,VAMAX,WAMAX - advection courant numbers (meters/
second).
UDMAX,VDMAX,WDMAX - diffusion courant numbers (meters/
second).

(14) /OUTF/ output unit numbers.
NUSP - spillet information.
NURS - restart data.
NUCN - concentration data.
NUPT - particle parameters.
NUMS - mass balance.
NULT - lost particle parameters.
NUDP - deposited particle parameters.
NUVL - velocity values.

(15) /PRNT/ control parameters for subsurface printout.
KPRTV,KPRTC,KPRTP - print control parameters for paper print-
out of velocity values, concentrations and particle
positions. This is an integer number which indicates
how often (in number of steps) the user wants this
information printed out. Value is zero if no print-
out is desired.
NPRD - control parameter to indicate that information is to
be written out to disk.
-0 for no writeout.
1 if any of the three variables below are not equal
to zero.
NPRV,NPRC,NPRD - control parameter for writing out to disk.
This indicates the interval (in number of steps)
between output to disk for velocity, concentration,
and particle position.
NPTSUB - controls printout of some subsurface information.
-1 no printout.
0 printout only the first timestep.
0 printout at that interval of steps.

(16) /PTYP/ - the particles are grouped into classes depending upon their
properties. This common block passes these properties.
NCLASS - number of classes at this timestep.
NUMBD(ICLASS) -(200) - number of particles in ICLASS.
DDIAM(ICLASS) -(200) - diameter of particle.
DDENZ(ICLASS) -(200) - density of particle. This is the
same density of the oil at the moment of entrainment.
(grams/cubic centimeter).
DMASS(ICLASS) -(200) - amount of mass represented by each
particle (metric tons).
DVELZ(ICLASS) -(200) - fall velocity of particle, usually is

- zero for neutrally buoyant oil droplet (meter/second).
- DCOMP(ICLASS,8) -(200,8) -composition of oil in the droplet. This is the composition of the oil at the moment of entrainment.
- NTCLASS - maximum number of classes allowed. This is currently set at 200.
- NUMCL - maximum number of particles in each class.
- (17) /SEAS/ - defines Sea State grid.
- MAXSX,MAXSY - number of grid elements in the X and Y direction.
- AS - angle between X axis and lines of constant Latitude (degrees).
- WAVHGT(MAXSX,MAXSY) -30,15 - average wave height (meters).
- WAVPRD(MAXSX,MAXSY) -30,15 - average wave period (seconds).
- XSL,YSL - Longitude and Latitude of (1,1) grid position.
- XSS,YSS - grid spacing in X and Y direction (meters or degrees).
- (18) /SHOR/ describes shoreline.
- NSHOR - number of shoreline points.
- XSHOR(ISHOR) -1500 - Longitude of shoreline points.
- YSHOR(ISHOR) -1500 - Latitude of shoreline points.
- (19) /SPIL/- passes spilllet properties.
- MSPIL - number of hydrocarbon fractions. This is currently set to eight.
- NSPIL - number of spilllets at this timestep.
- ASPIL(ISPIL) -99 - treated area of spilllet. This is negative when the total spilllet has been treated (meters²).
- BSPIL(ISPIL) -99 - time that spilllet appeared (seconds).
- DSPIL(ISPIL) -99 - density of spilllet (grams/cubic centimeter).
- FSFIL(ISPIL) -99 - fraction by volume of treated spilllet.
- GSPIL(ISPIL,MSPIL) -(99,8) - fraction by mass of each hydrocarbon class for the spilled oil.
- RSPIL(ISPIL) -99 - radius of spilllet (meters).
- SSPILT(ISPIL) -99 - interfacial tension of oil (dynes/centimeter).
- SSPILT(ISPIL) -99 - interfacial tension of treated oil (dynes/centimeter).
- TSPIL(ISPIL) -99 - not used
- TSPILT(ISPIL) -99 - not used
- USPIL(ISPIL) -99 - kinematic viscosity of the oil (centistokes).
- WSPIL(ISPIL) -99 - mass of the oil in spilllet (metric tons).
- XSPIL(ISPIL) -99 - Longitude at center of a spilllet.
- YSPIL(ISPIL) -99 - Latitude at center of a spilllet.
- (20) /SUBS/- control parameters for subsurface section.
- NTRANS - transforms the Z direction.
- 0 uses depths as given.
- 1 transforms Z so that all Z values are normalized by the depth.

NSUB - 0 particle diffusion with respect to Lagrangian grid.
1 use analytical diffusion until standard deviation of cloud is comparable to grid mesh.

NEXTR - control of Lagrangian grid.
0 use fixed grid.
1 use expanding and translating grid.

NMAX - maximum number of particles. Restricted by dimension of particle location variables.

NMAX - number of particles at current timestep.

DX,DY,DZ - grid spacings of Lagrangian grid (meters or degrees).

XORIG,YORIG - this is the distance between the origin of the fixed depth grid and the floating Lagrangian grid. These numbers are in fixed depth grid units. Therefore, to get the actual distance in meters or degrees, these numbers must be multiplied by the grid spacing of the depth grid (XDS,YDS).

ZORIG - point of reference for vertical distances. For a constant depth, this is at the bottom.

(21) /TIDE/ - Advective current grid. There are two grids, one for X velocities and one for Y velocities. They have the same spacing, size, and orientation but may have different origins so that a numerical model using a space staggered grid may be used to generate the values.

MAXTX,MAXTY - number of grid elements in the X and Y direction.

AT - angle between X axis and lines of constant Latitude (degrees).

UT(MAXTS,MAXTY) -30,15 - velocities in the X direction (meters/second or degrees/second).

VT(MAXTX,MAXTY) -30,15 - velocities in the Y direction (meters/second or degrees/second).

XTLU,XTLV - Longitude of (1,1) grid position for UT and VT.

YTLV,XTLV - Latitude of (1,1) grid position for UT and VT.

XTS,YTS - grid spacing in X and Y directions for both tidal current grids (meters or degrees).

(22) /TMPC/ - temperature grid.

MAXKX,MAXKY - number of grid elements in the X and Y direction.

AK - angle between X axis and lines of constant Latitude (degrees).

TEMP(MAXKX,MAXKY) -30,15 - temperature (degrees centigrade).

XKL,YKL - Longitude and Latitude of (1,1) grid position.

XKS,YKS - grid spacing in X and Y direction (meters or degrees).

(23) /WIND/ - wind grid

MAXWX,MAXWY - number of grid elements in the X and Y directions.

AW - angle between X axis and lines of constant Latitude (degrees).

UW(MAXWX,MAXWY) -30,15 - wind speed in X direction (meters/

second).
VX(MAXWX) -30,15 - wind speed in Y direction (meters/
second).
XWL,YWL - Longitude and Latitude of (1,1) grid position.
XWS,YWS - grid spacing in X and Y directions (meters or
degrees).

APPENDIX IV: PROGRAM SUBROUTINE AND ALGORITHM DESCRIPTIONS FOR
THE SIMULATION MODEL

This Appendix is devoted to the detailed description of the main program and each of the subroutines of the simulation model. The main program is discussed first, and then followed by the subroutines in alphabetical order. Following the description of each subroutine is a list, including a description of the subroutine's most important arguments which are not in common or read in. Those variables in common or read in have been discussed in Appendices II and III.

1. Main Section

The main section of the program acts as the controller for a simulation. All of the major subroutine calls originate from this section. Initialization for all but the subsurface variables is performed by this section and it controls all input by either reading the variables directly or by calling the subroutines which then do the reading. (See Figure IV-1). Following the standard initiation at the run control parameters, there may be a second level of initialization controlled by the parameter NSTRT. This initialization occurs if NSTRT equals one, i.e., if this run is to be a continuation of a previous one. If NSTRT equals zero, this section is skipped.

The restart section will read all previous output data sets to their end and then it will read the restart data set which locates all spillets and determines the mass and subsurface parameters at the last step for which restart data was written. The previous environmental, spillet, cleanup and treatment efforts are read in under control of the parameter INR which counts the steps up to the restart step. The same input data sets used for the restart are the ones used for the previous run which did not finish. The same output data sets will be used as well. If the user desires to use new input and output data sets for the restarted run, the input variable NSTFN must be set equal to zero. Care should be taken when using new data sets to be sure the new unit numbers and/or data set names should be correct in the input data set.

The next major section of the program consists of the iteration over time. This is the actual simulation of the spill. This begins with the input of the step control parameters. The formatted printout of the commands issued by the step control parameters is determined by the input variable NENV, which indicates the step interval for output. Following this step, the program reads the appropriate environmental variables, spillets and cleanup activities and then performs the indicated cleanup operations. The main surface subroutine (SURFUS) and main subsurface routine (SUBSUR) are then accessed. Prior to calling the subsurface routines, the program converts all verticle measurements to the transformed system if required (no transformation for NTRANS = 0, transformation for NTRANS = 1).

In the next section, the mass balance is calculated and any spillets that overlap by a predefined fraction (COMB) are combined regardless of the step number. The last function performed for a time sep is to write to disk the restart data if the step number is a multiple of NSUMM or if this is the last time step of the run. If this is not the last time step, the entire simulation procedure is repeated from the entry of the step control parameters.

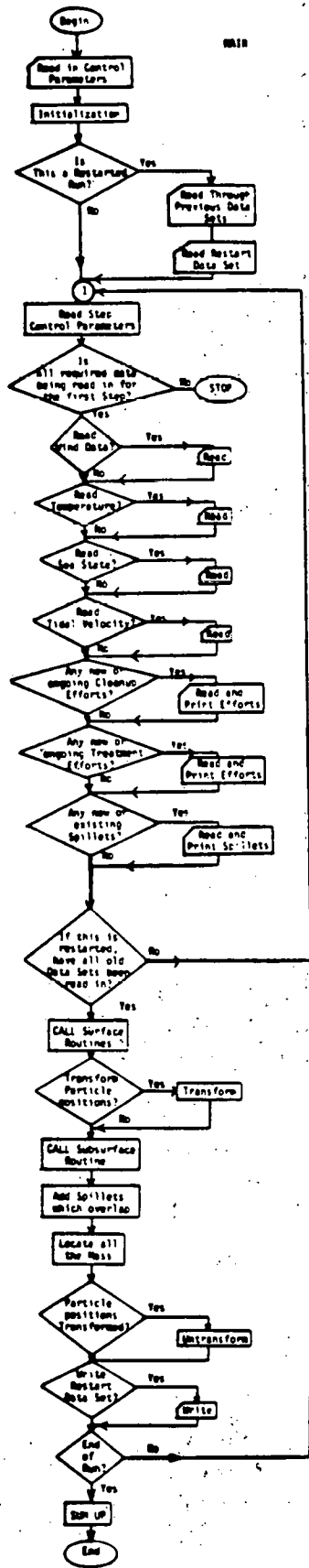


Figure IV - 1. Flowchart for sedimentation RLII.

SUBROUTINES CALLED: ADD, ARAYIN, BOTDFT, CHEMIN, CLNIN,
 CNVRTZ, CONSUM INITSS, MASSC, READF,
 READI, RESRFS, SHORE, SPILIN, SUBSUR,
 SUMMUP, SURFES.

Important Variables Not in Common Read In

- INR - This is used for the restart section. It counts the number of times that the program reads through the environmental input parameters before it has come to the step at which the previous run terminated.

- NSTEP - Step number. Time zero is step zero.

- NORDR (ICLASS) - 2000 Integer *2 - Class to which that particle belongs.

- X,Y,Z (I) - 2000 - Position of droplet with respect to origin of floating grid (meters or degrees).

Subroutine ADD

This subroutine combines two spilletts and their properties if they overlap by more than some predetermined fraction. (See Figure IV-2). The sum of their radii is compared to the distance between the centers. If this difference is larger than a given percentage (defined by input the parameter COMB) of the smallest of the two radii, then they are combined. Spillet parameters of the two spilletts are combined either by adding the two values or by calculating a weighted average of the two. For example, the mass is simply the sum of the two while the location is a weighted mean (by weight) of the location of the two centers. In Table IV-1, all spillet variables are listed along with the method of combination.

CALLED FROM: MAIN

SUBROUTINES CALLED: DIST

Important Variables not in Common or Read in:

- DISTA - the sum of the radii.

- DIS - distance between spillet centers.

- NSAV(ISP) - 99 - number of the spillet which has been moved to the end of the list.

ADD

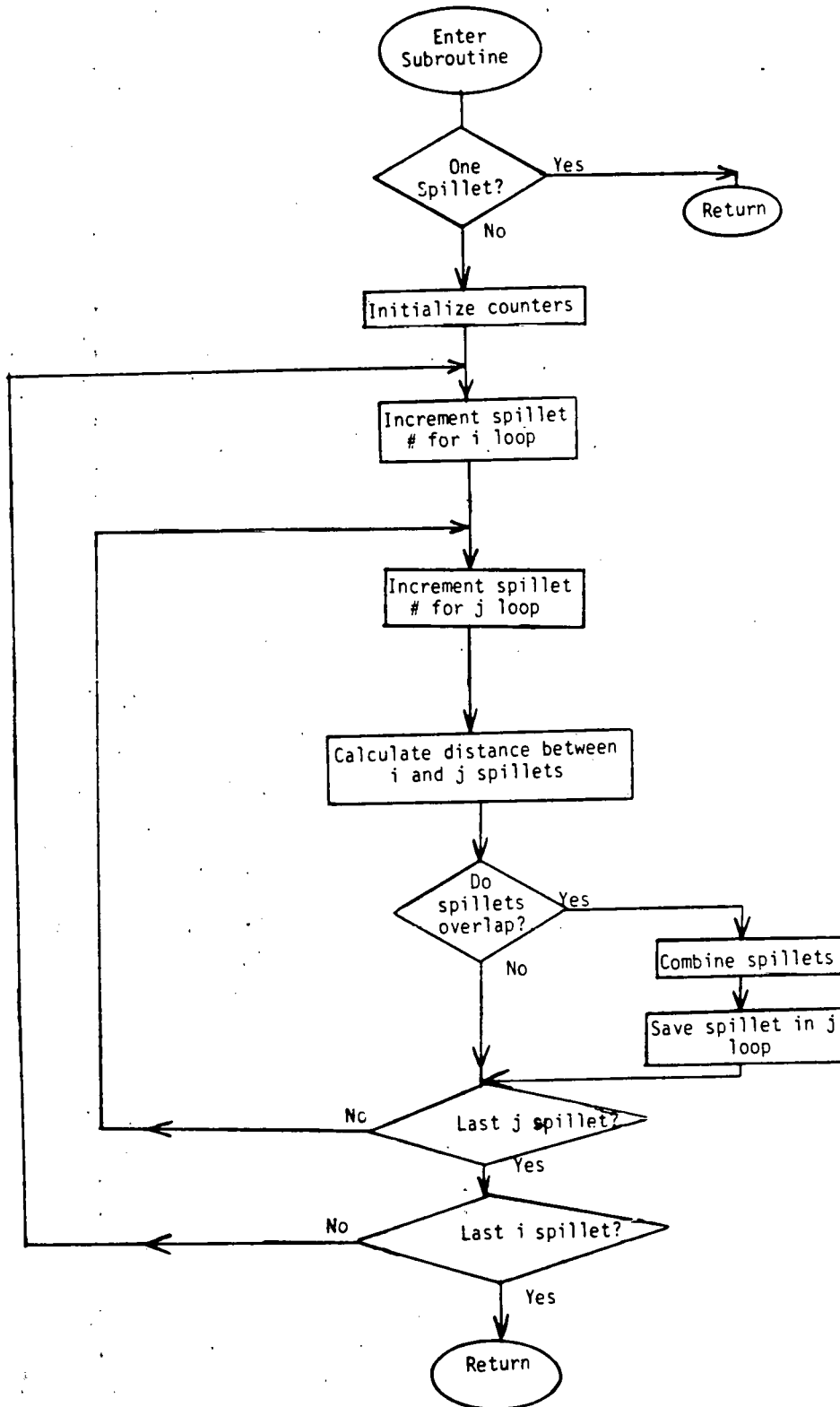


Figure IV - 2. Flowchart for subroutine ADD.

Table IV-1

Combination of Spillet Parameters in Subroutine ADD

<u>Variable Name</u>	<u>Method of Combination</u>	<u>Variable Description</u>
ASPIL	Sum	Spillet area treated
GSPIL	Weighted mean	Fraction by mass of each class of oil
RSPIL	Square root of sum of squares, i.e., sum areas	Spillet radius
SSPIL	Weighted mean	Interfacial tension of oil
TSPIL	Weighted mean	Density of oil at $t=0$
SSPILT	Weighted mean	Interfacial tension of Treated oil
TSPILT	Weighted mean	Not used
USPIL	Weighted mean	Kinematic viscosity of oil
USPIL	Sum	Mass of oil in spillet
XSPIL	Weighted mean	Longitude of spillet center
YSPIL	Weighted mean	Latitude of spillet center
FSPIL	Weighted mean	Fraction by mass of treated spillet

Subroutine ARAYIN

This subroutine has been designed to enter all environmental grids. It is flexible in that the orientation, size and location of each grid may be different but structured in that the defining parameters must follow one of a number of well-defined formats. The precise format statements, as well as the various formatting options are described in detail in Appendix I, along with associated variables. In this section, the operation of the subroutine is discussed in terms of the flow diagram, Figure IV-3.

Upon entering the subroutine, the grid definition parameters are read either formatted or unformatted, depending on the value of the format control parameter NU. The dimensions of the grid are then verified. If ISCAL equals 1, then the grid separation is in meters and must be larger than 5 or the program stops. If, on the other hand, ISCAL equals 2, the grid separation is in spherical coordinates and must be less than or equal to 5 or again the program stops. Finally, if the grid separation is in spherical coordinates, the grid cannot be rotated so the parameter ANGLE must equal zero. If it is not, the program stops. If all of the conditions are successfully met, the grid may be printed out if desired. This printout is controlled by NPRTA, (-1 no printout, 0 limited printout and 1 full printout).

The next step is to read in the environmental parameters. First the format type is determined, real formatted, real unformatted, integer formatted or integer unformatted and then the first variable is input for the entire grid. If there is a second variable, NO equal to 2, it is then input. The last step is to output the environmental data again under control of NPRTA.

CALLED FROM: MAIN

SUBROUTINES CALLED: NONE

Important Variables Not in Common or Read In See Table I-1

Subroutine AVGSIG

This subroutine calculates the average of the particle positions (X,Y,Z) over all particles then, under control of NCELCT, calculates the standard deviation. The standard deviation is defined by:

$$\sigma = \sqrt{\frac{\left[\sum_{i=1}^N x_i^2 - \left(\frac{\sum_{i=1}^N x_i}{N} \right)^2 \right]}{N - 1}}$$

CALLED FROM: DIFF, DISPV

SUBROUTINES CALLED: NONE

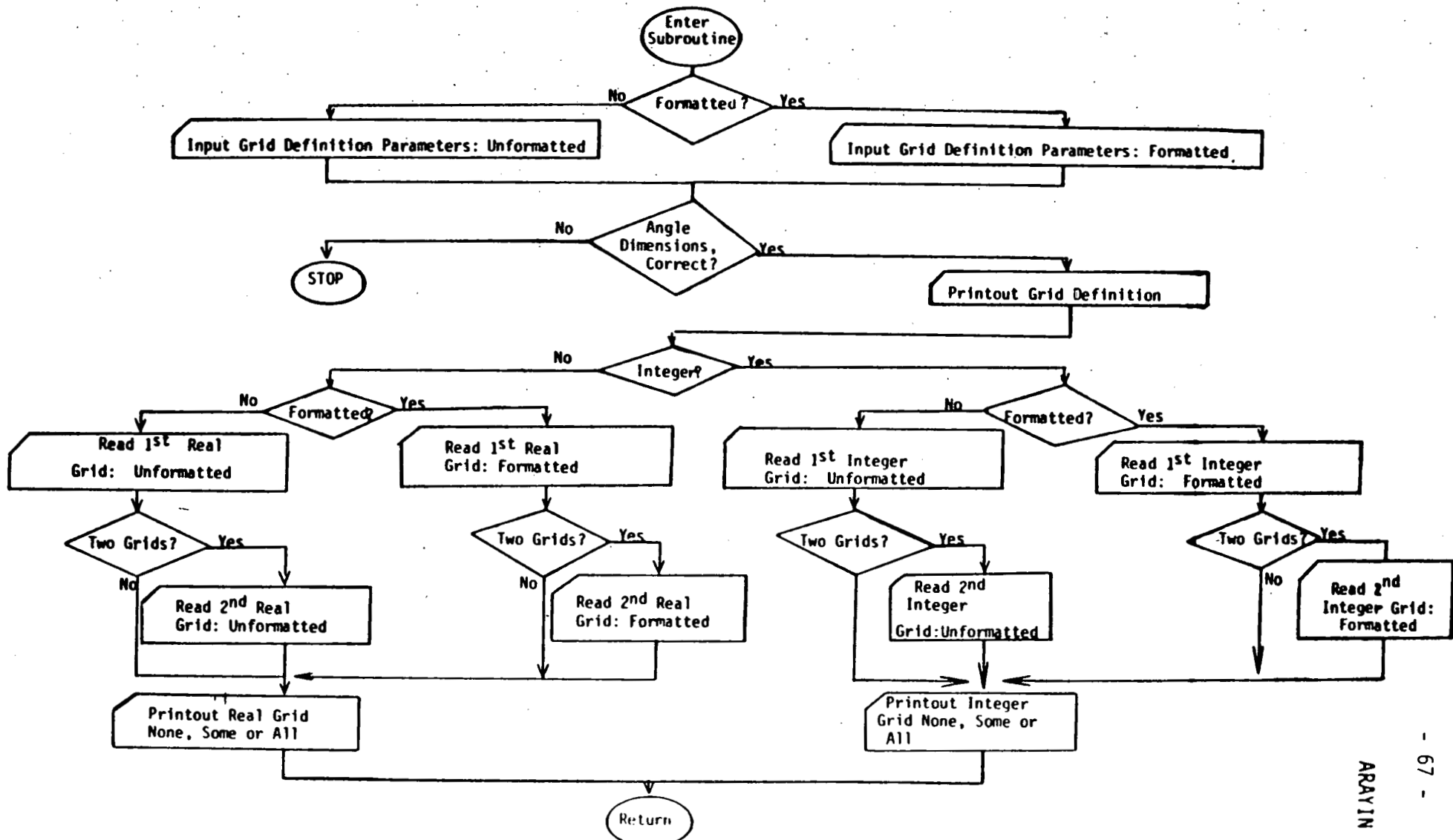


Figure IV.-3 Flow Chart for subroutine ARAYIN

ARAYIN

Important Variables not in Common or Read in

- XNUM - number of particles
- XAVG, YAVG, ZAVG - average values for X, Y and Z positions.
- SIGX, SIGY, SIGZ - standard deviations of X, Y and Z positions.
- NCELECT - 0 calculate only the mean.
- 1 calculate the mean and standard deviation.

Subroutine BOUNV

This subroutine locates the position of the particles with respect to the computational cell grid and then, either displaces the particle, removes it from the particle list, or leaves it as it was, depending on the numerical value of the computational cell grid element in which it is located. See Figure IV-4, for a flow chart of BOUNV.

First, the routine determines where each of the floating grid nodes are with respect to the fixed computational grid. Each floating grid element is then assigned the boundary condition of the fixed computational grid in which it is located. The number associated with each condition is listed in Table IV-2. The particles are then located within the floating grid. If a particle is within one half of a grid distance of an open boundary or a bottom deposition cell, the particle is removed from the list. If the grid is a reflection cell, the program moves the particle to half of a grid space, plus a small distance (ER) away from the boundary. The user can change the value of ER within the program. A particle occupies a fictitious cell volume, equal to a floating grid cell, so the boundary calculations are determined by the overlap of this particle volume in the boundary cells. If the particle is deposited or lost, the last particle on the list is moved to its position in the order. At present, the land cells are generally defined as reflection cells as are the surface boundary cells. The user may, however, assign any configuration to these that s/he desires.

The location and properties of any droplet deposited or lost are written to a disk data set. The number of particles either lost or deposited are printed out by the MASSC subroutine.

CALLED FROM: SUBSUR, PRINT

SUBROUTINES CALLED: ROTAT

Important Variables not in Common or Read In

- ER - When a particle is moved, it is moved this fraction of a grid cell beyond the middle of the cell.
- M - I, J, K - The boundary conditions of the floating grid location calculated from the fixed computational cell grid. See Table IV-2 for the meaning of the various numerical values.

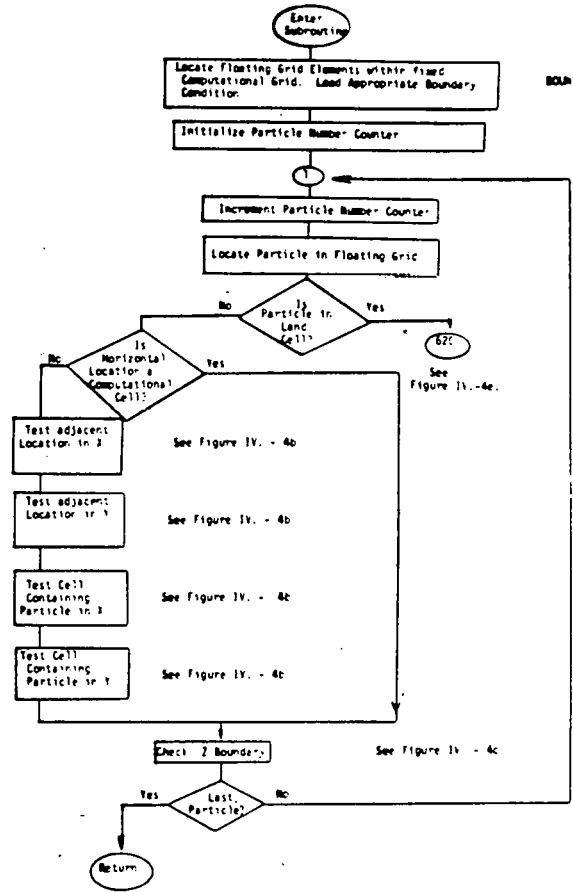


Figure IV.-4e. Flow Chart for Subroutine BOUND

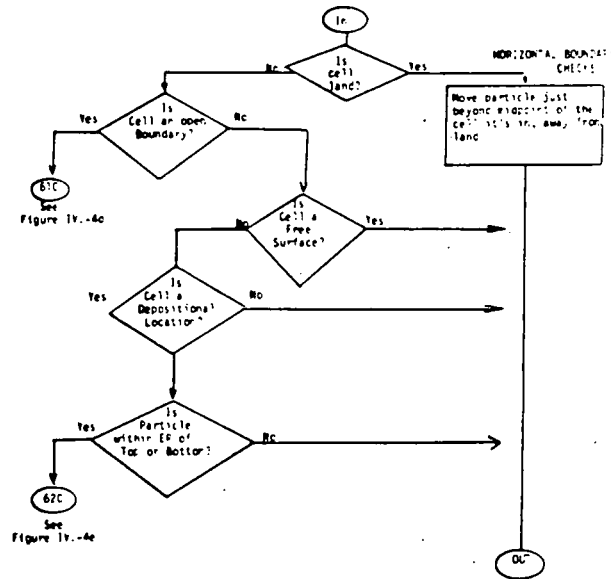


Figure IV.-4b. Flow Chart of Horizontal Boundary Checks

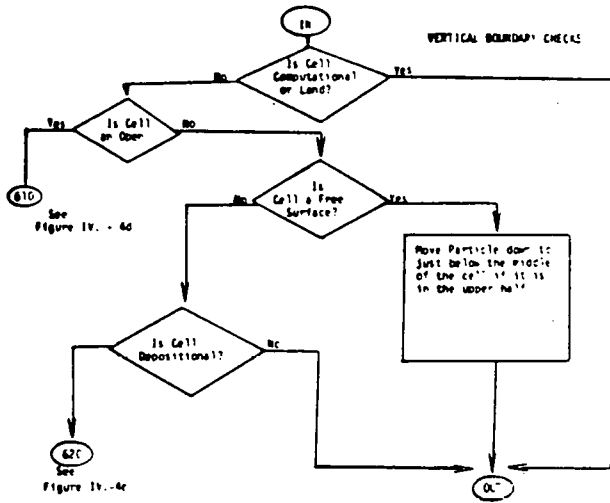


Figure IV - 4c. Flow Chart of Vertical Boundary Checks

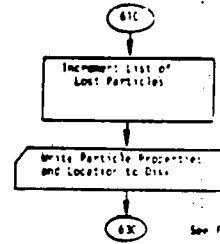


Figure IV - 4d. Flow Chart of Lost Particle Operator

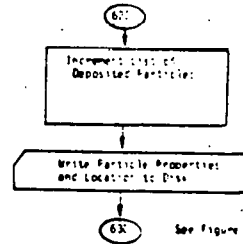


Figure IV - 4e. Flow Chart of Deposited Particle Operator

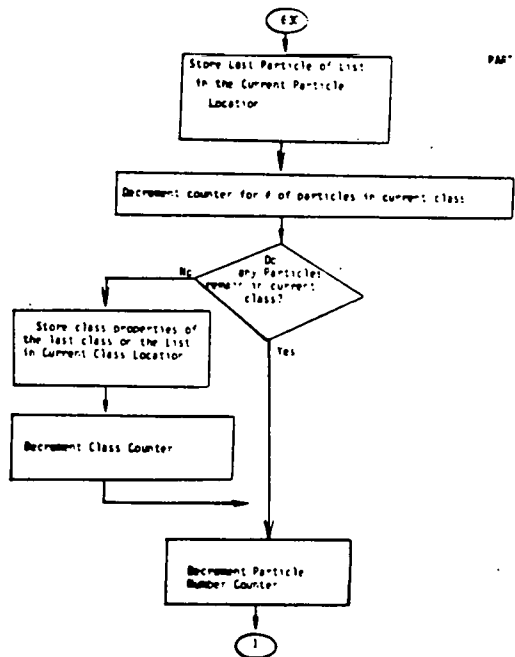


Figure IV - 4f. Flow Chart of Particle Removal.

Table IV-2
Model Boundary Conditions

DEFINITION	VALUE	ACTION TAKEN
Land Cell	0	Deposit particle, remove particle from list
Computational Cell	1	none
Open boundary	2	remove particle from list
Water cell with an adjacent cell that is not water	101	none
Free surface reflection cell	3	Displace particle down if in the lower half of the cell
Bottom Deposition Cell	4	Absorbs any oil which moves to within 1/2 grid spacing of bottom.

Subroutine CHEMIN

This subroutine reads in the data for new chemical treatment efforts and also lists all treatment efforts in progress. See Appendix I for a description of the input format and see Figure IV-5 for a flow chart of this subroutine.

The subroutine first prints a header. Then all efforts in progress are listed. Finally, new efforts are read in and their characteristics pointed out.

CALL FROM: MAIN

SUBROUTINES CALLED: NONE

Important Variables not in Common or Read In: None

Subroutine CLNIN

This subroutine serves two functions: It reads in the data that determines new mechanical cleanup efforts and it lists all mechanical cleanup efforts in progress. See Appendix I for a description of the input format and See Figure IV-6 for a flow chart of this subroutine.

First, the subroutine prints a header. Then all efforts in progress are listed. Finally, new effort(s) are read in and their characteristics printed out.

CALLED FROM: MAIN

SUBROUTINES CALLED: NONE

Important Variables not in Common or Read In: None

Subroutine CLNUP

This subroutine simulates the mechanical cleanup of spilled oil. See Figure IV-7. At any one time, there may be up to ten individual cleanup efforts in progress. Each effort is defined by its location, radius of influence, beginning time, duration, oil recovery rate and efficiency of cleanup effort. This last variable is to simulate the possible inability of the cleanup device to remove all of the oil in a spillet from the surface.

The subroutine is called once for each spillet every time step as long as there are continuing cleanup efforts. The first function performed is to remove any expired cleanup efforts from the list. This is done by subroutine REMOV. Following this, each of the cleanup efforts is examined in sequence to determine whether or not its range of influence includes the current spillet. If it does, a volume of oil is removed from that spillet equal to the smaller of:

1. The cleanup rate times the time step.

CHEMIN

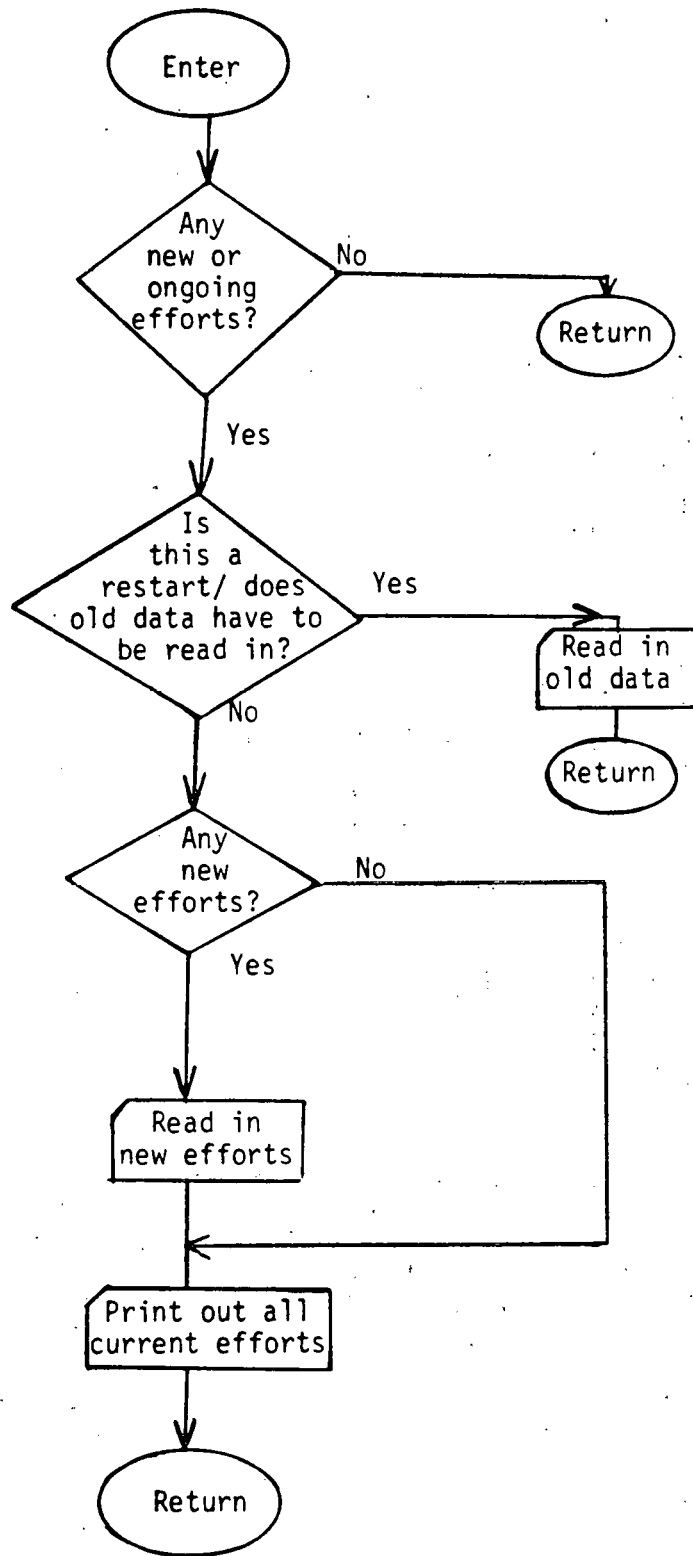


Figure IV - 5. Flow chart for subroutine CHEMIN.

CLNIN

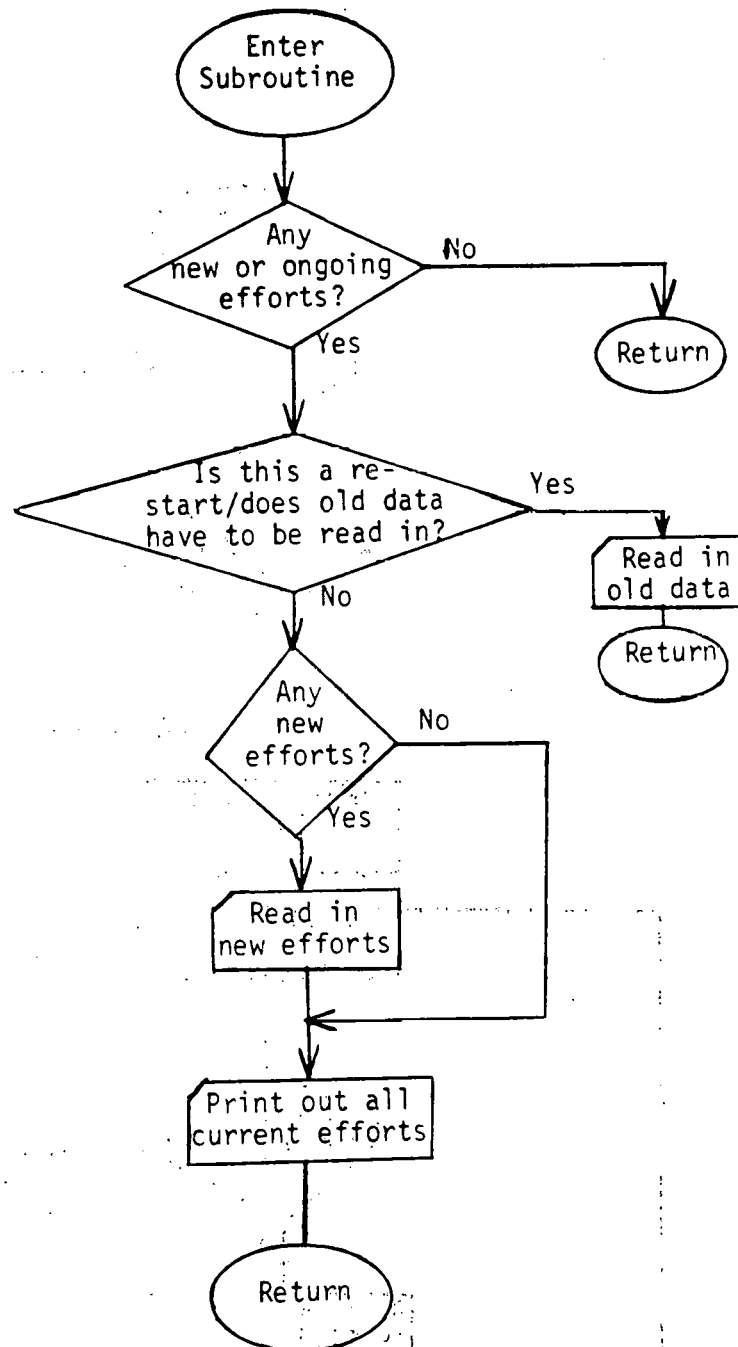


Figure IV.- 6. Flow chart for Subroutine CLNIN.

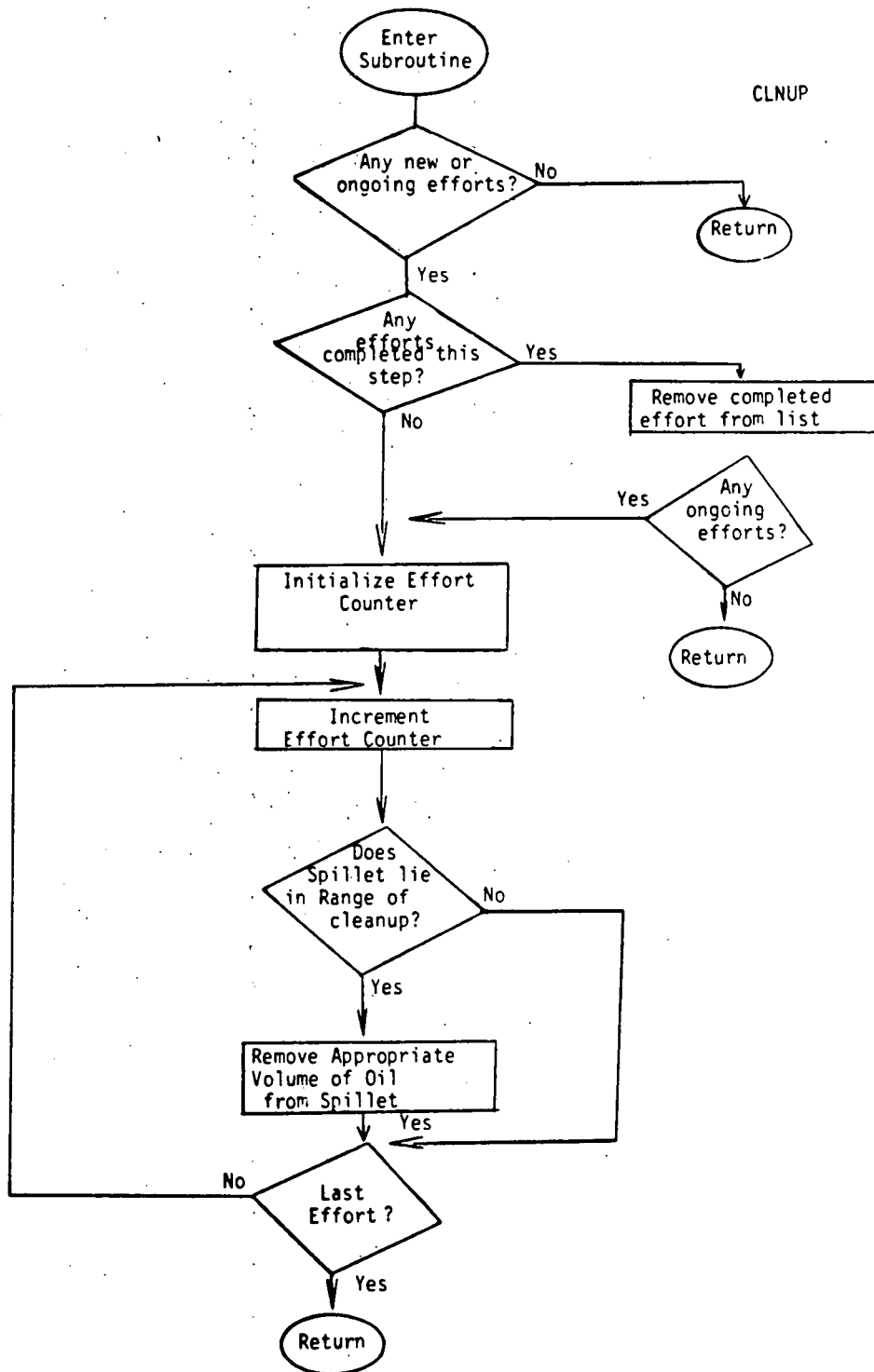


Figure IV.7. Flow Chart for Subroutine CLNUP.

2. The total volume of the spilllet times the efficiency factor.

Following any action by all current cleanup efforts, the mass balance of the spill is updated and control is returned to the main program.

It should be noted that the volume cleanup rate of a particular effort applies to each spilllet the center of which falls in the area covered by that effort. This means that if three spilllets fall within the range of a given cleanup effort, a maximum of three times the volume cleanup rate for that effort may be removed from the surface.

CALLED FROM: MAIN, SURFES

SUBROUTINES CALLED: REMOV, DIST

CLNUP VARIABLES

- ISP - the number of spilllet on which the cleanup efforts is operating.
- SMCLN - Amount of oil removed from this spilllet (metric tons).
- RC - Radius of spilllet, ISP (meters).
- DIS - Distance between center of cleanup effort and center of spilllet (meters).
- AMNT - Maximum amount of oil which may be removed in this step (metric tons).
- EFF - Efficiency expressed as a fraction.

Subroutine CNVRTZ

This subroutine, Figure IV-8, converts the particle positions in z, the vertical coordinate, to or from the transformed coordinate system. This transform is regulated by the parameter NTRANS (see input variables). If NTRANS = 1, this routine is called at the beginning and end of the run. The transformation consists of interpolating the water depth at the particle position from the depth grid, and then normalizing the z position by this depth. The result is that the relative resolution in z is independent of horizontal location (x,y).

CALLED FROM: MAIN

SUBROUTINE CALLED: VELC

Important Variables not in Common or Read In

- MONTRL = -1 convert from transformed system.
- = 1 convert to transformed system.

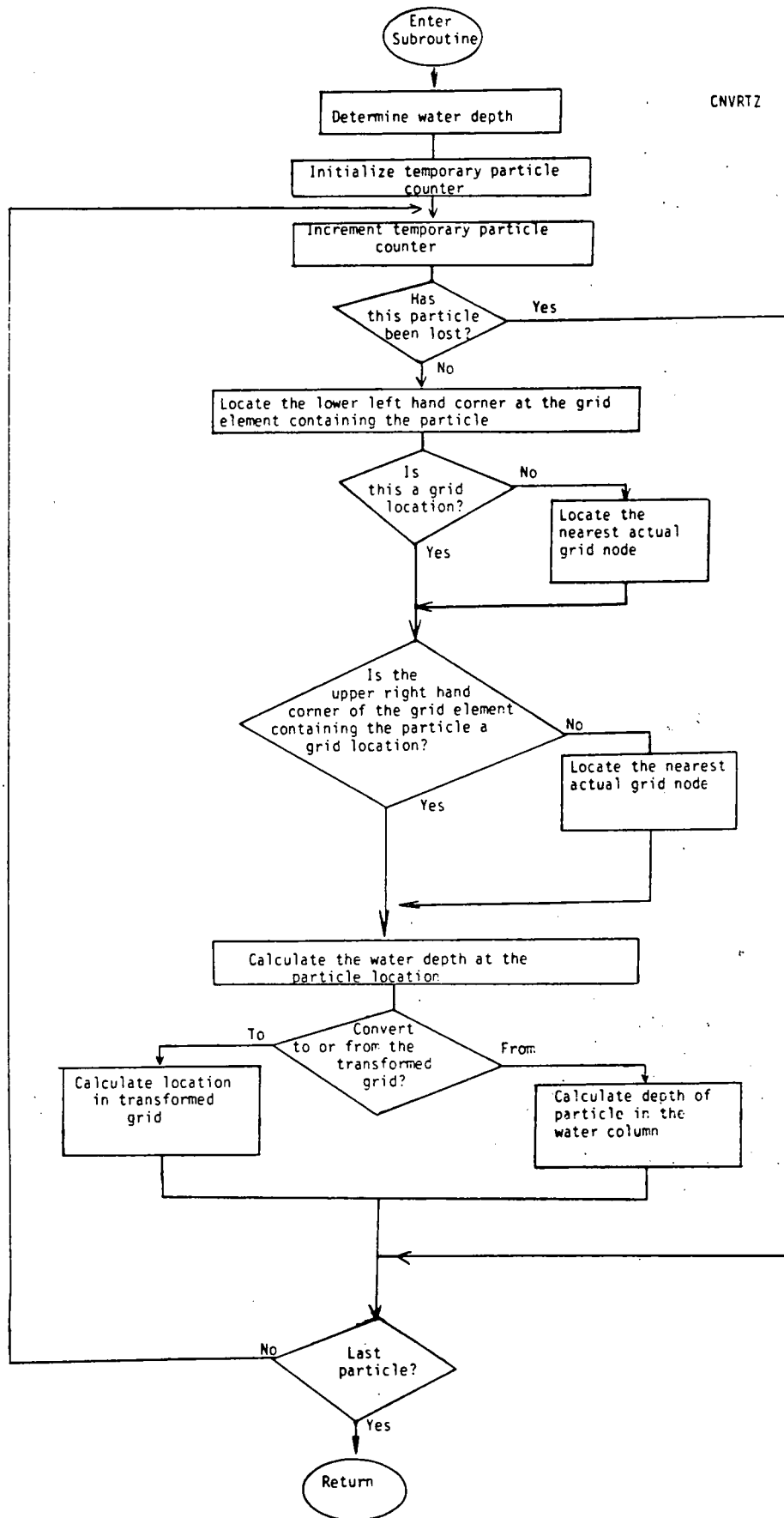


Figure IV. 8. Flow Chart for Subroutine CNVRTZ

Subroutine CONC

This subroutine (Figure IV-9) determines the hydrocarbon concentration in the water column resulting from entrainment. Each particle is assigned a fictitious volume equal to the volume of a floating grid element and centered on the particle location. The fraction of this volume in each floating grid element is then added to the volume of oil already in that element. The fictitious volume may overlap a maximum of eight surrounding cells. This process is performed for each particle. When all particles have been processed, the mass of oil in each floating grid element is divided by the volume of that element to determine the concentration.

CALLED FROM: SUBSUR, PRINT

SUBROUTINES CALLED: None

Important Local Variable: none

Subroutine COURAN

This subroutine, see Figure IV-10 for its flow chart, is used to determine when the courant condition has been violated. The courant condition specifies that a marker particle may not move more than one half of a model grid unit in one time step. If the condition is violated, the numerical results are uncertain and a message to that effect is printed out. The run will continue. In the early stages of a spill, the courant condition will often be violated. Because the floating grid dimensions are small, the surface spillet is small, but the time step is relatively long. It is thought that for the simulation of the model in its present form, this problem is not overly serious because it is the long term results that are of interest. The early stage instabilities have little effect on these results. If it is the near term results that are being examined, then the time scale must be considerably shortened compared to the values used in the examples of this manual.

Two sets of courant numbers have been defined, one for the advective velocity component and one for the diffusive velocity component. This is because the fixed grid on which the advective velocities are defined is generally much larger than the floating grid on which the diffusive velocities are defined. It is, therefore, conceivable that the courant condition is not violated even though a marker particle moves several floating grid units.

CALLED FROM: SUBSUR

SUBROUTINES CALLED: None

Important Local Variables:

CAU - courant number for advective velocity in x.

CAV - courant number for advective velocity in y.

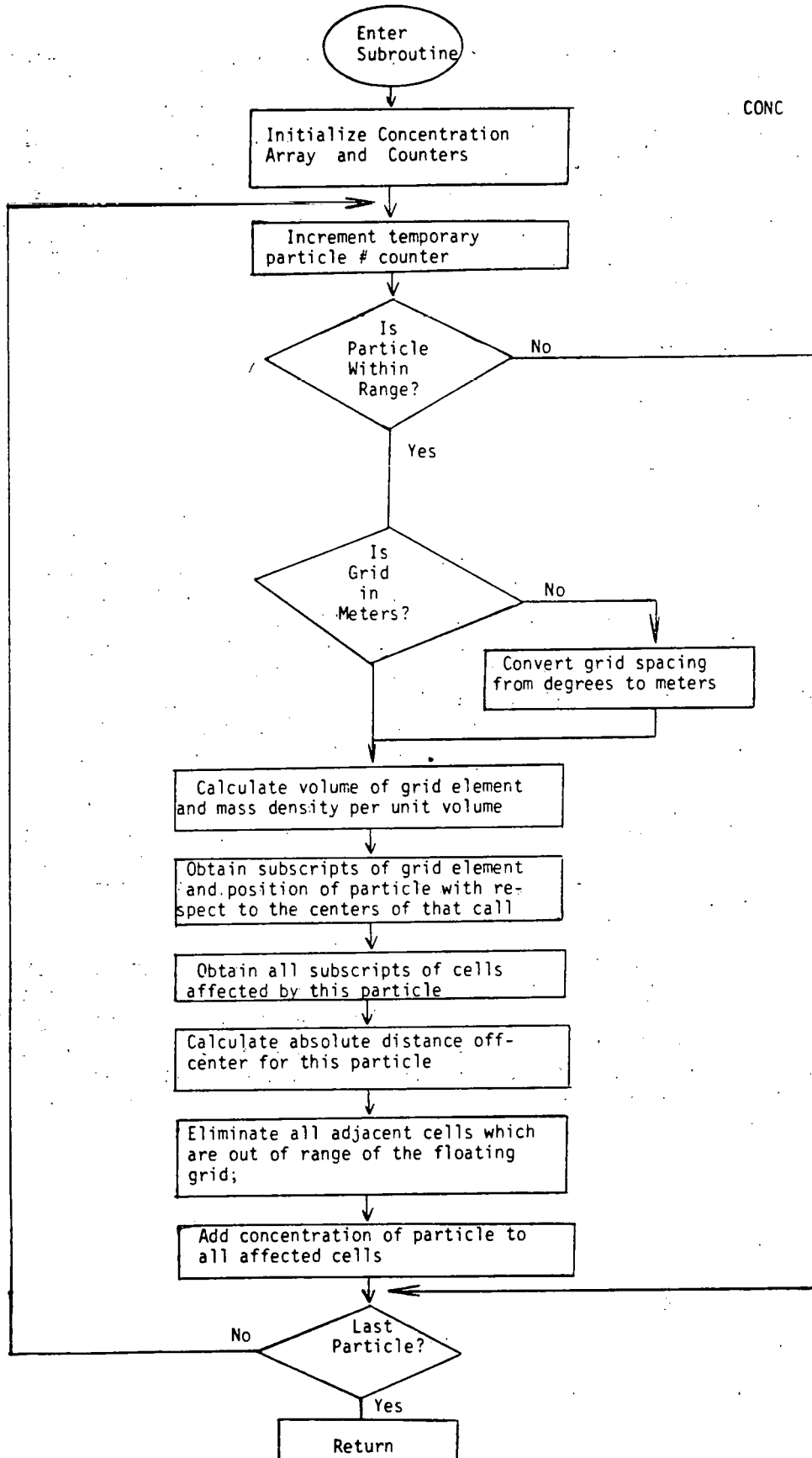


Figure IV.-9 Flowchart for Subroutine CONC.

COURAN

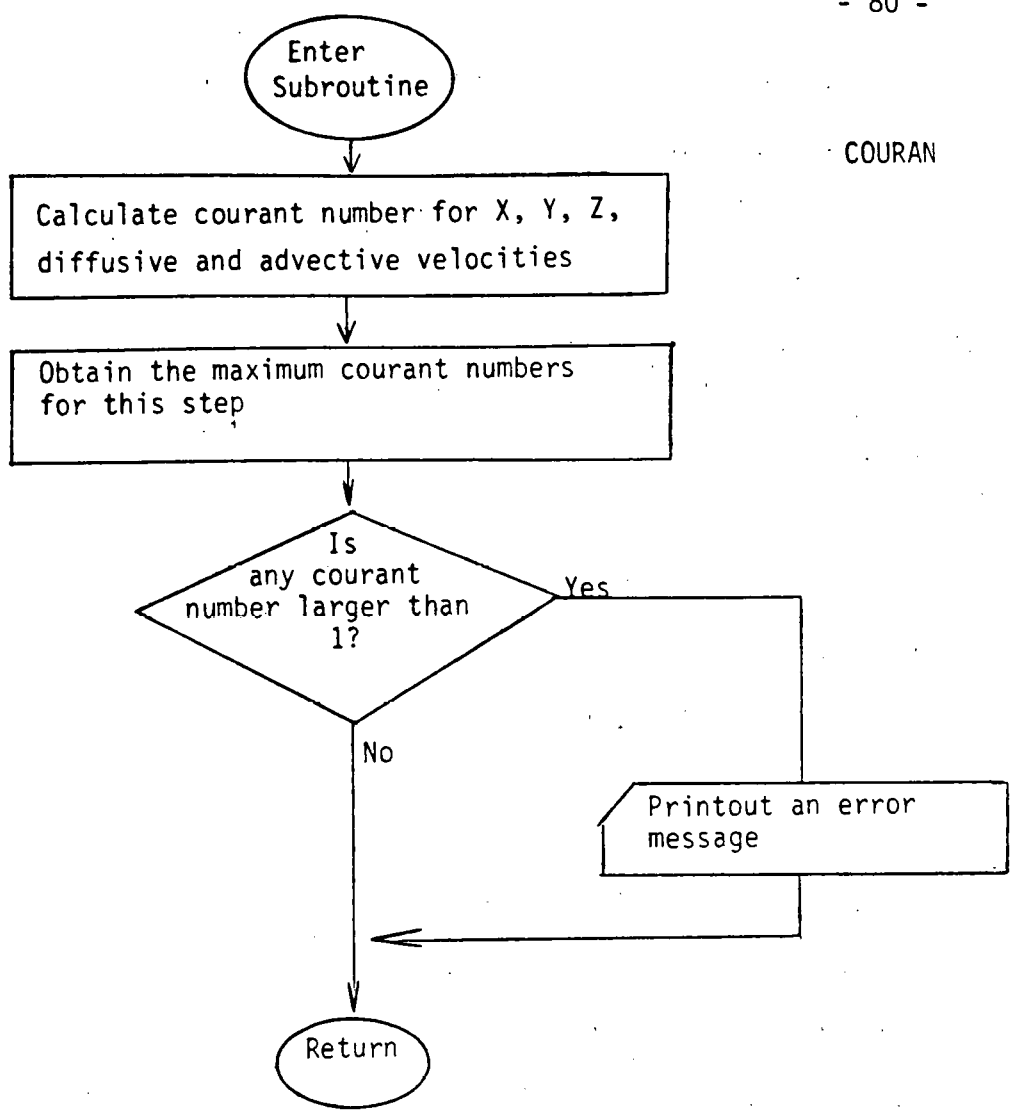


Figure IV.-10. Flow Chart for subroutine COURAN.

CAW - courant number for advective velocity in z.

CDU - courant number for diffusive velocity in x.

CDV - courant number for diffusive velocity in y.

CDW - courant number for diffusive velocity in z.

Subroutine DIFF

This subroutine (Figure IV-11) calculates the diffusion coefficient if the scale dependent diffusion model has been selected (see input parameter NDIFF). It uses subroutine AVGSIG to calculate the standard deviations of the particle positions and then the 4/3 law to determine the coefficient. If the large scale mode is used, the diffusion coefficient is calculated for the average latitude of the droplet cloud. The X component of the diffusive coefficient is given by:

$$DXX = EXX * SL^{POWX}$$

where $SL = 3.0 * 2.0 * SIGX * SIGY$

SIGX, SIGY are the standard deviations of the particles.

DXX - diffusion coefficient (m^2/sec).

EXX - constant. (now set to .05)

POWX - constant. (now set to 4/3)

The y and z components are determined in a similar fashion. The values for the scale-dependent diffusion coefficients can come from Pavish and Spaulding (1977). The value for POWX and POWY is recommended as .99838 (assuming the length scale is in meters). The coefficient (EXX) is .0018. This is a composite line from many sources of data including Okubo, Yudelson, Kohand, and Chano.

CALLED FROM: SUBSUR, VELCT

SUBROUTINE CALLED: AVGSIG

Important Local Variables: as above

Subroutine DISPV

This routine (figure IV-12) displaces each particle according to the advective and diffusive velocities calculated for the timestep being simulated. The velocities of the particle are calculated by the routine PARTV. The distance that a given particle is displaced is equal to the particle velocity times the length of the timestep.

CALLED FROM: SUBSUR

SUBROUTINE CALLED: AVGSIG

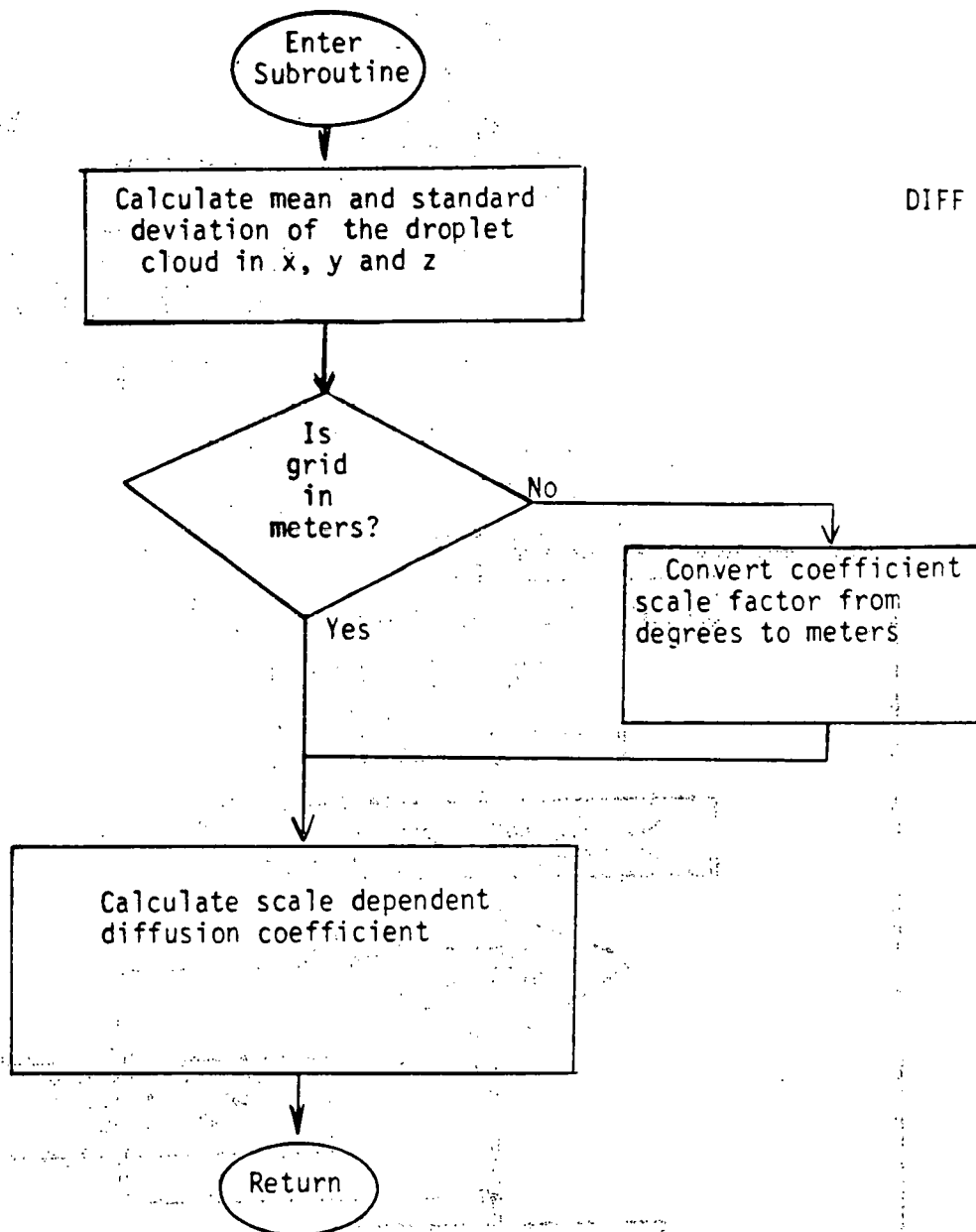


Figure IV. -11. Flow Chart for subroutine DIFF.

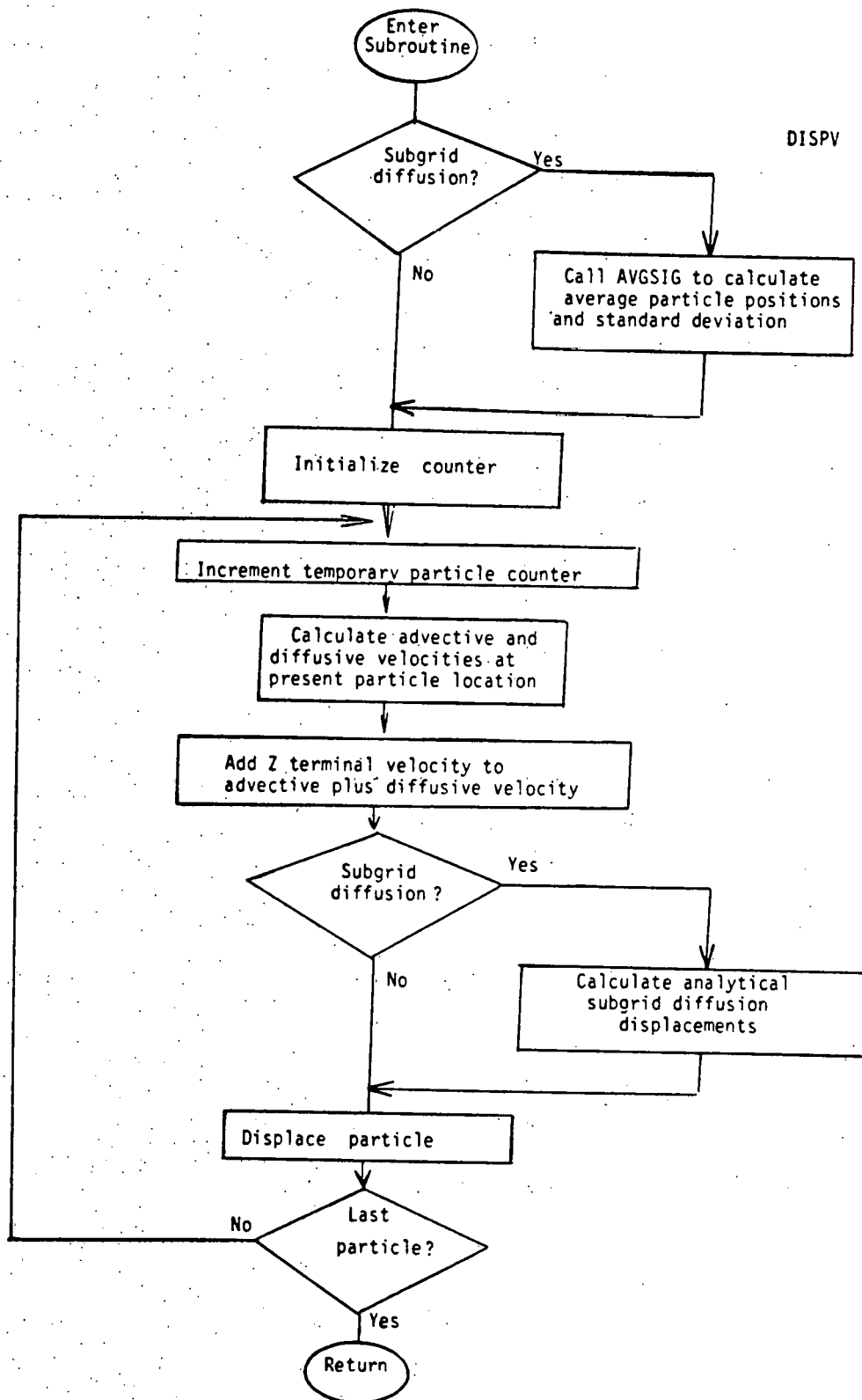


Figure IV - 12. Flow Chart for subroutine DISPV

Important Local Variables:

DFLT-depth of water at floating grid locations

HFLT-sea surface evaluation at floating grid locations.

Subroutine DIST

This subroutine, see Figure IV-13 for its flow chart, is used to calculate the horizontal separation between any pair of points. The separation is always returned either in meters or in degrees as determined by the control parameter NO. If NO is equal to either 2 or 5, the values returned are the x and y separation in the rectangular coordinate system locally aligned with lines of constant longitude and latitude. If NO is other than 2 or 5, the great circle distance between the two points is returned. The distinction between a value of 2 or 5 for NO stems from two different storage modes for point locations. If NO equals 2, the input locations are assumed to be in longitude and latitude and the result is returned in meters. If NO equals 5, no conversion is performed so if the input is in meters, so is the output.

CALLED FROM: ADD, CLNUP, ENTRN, LOC8, ROTAT, TREAT

SUBROUTINES CALLED: None

Important Local Variables:

X1,Y1 - longitude and latitude of the first point. This point should be south and west of the second point.

X2,Y2 = longitude and latitude of the second point.

NO = 1 calculate the great circle distance between the points (meters).

= 2 calculate the X and Y spacing between the points (meters).

= 5 calculate the X and Y spacing between the points in the same units as the input.

ANG - angle if one point is defined on a rotated grid.

D - distance between the two points if NO=1.

XSP,YSP distance between the two points if NO=2 or 5.

Subroutine ENTMAS

This subroutine, see Figure IV-14 for its flow chart, calculates the mass entrained under natural conditions, i.e. no dispersant. It uses the rate obtained by the formulation of Andunson (1979). Specifically, the

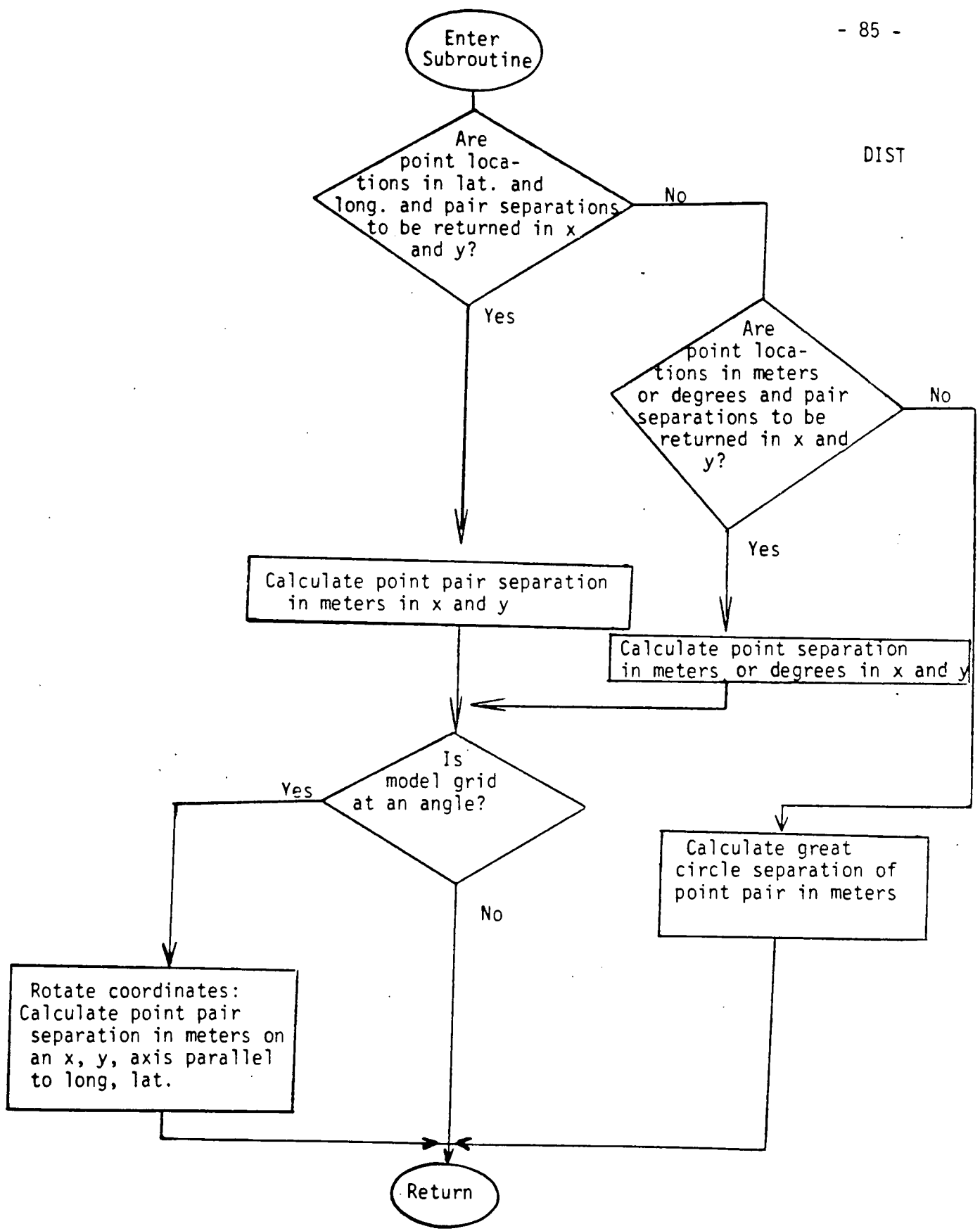


Figure IV. - 13. Flow Chart of subroutine DIST.

ENTMASS

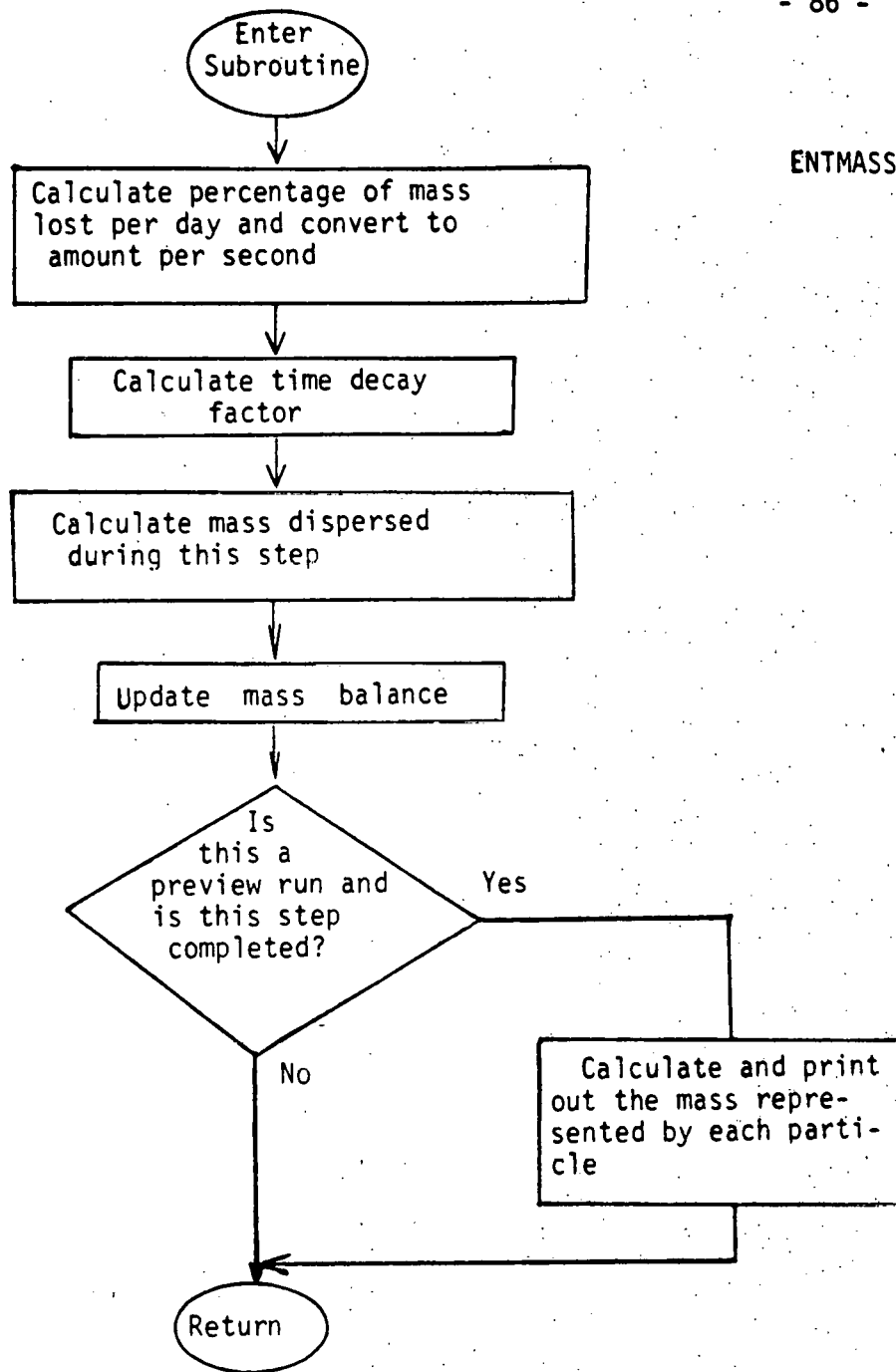


Figure IV - 14. Flow Chart for subroutine ENTMASS.

fraction of oil entrained per day is given by:

$$\text{Amount} = 0.1 \frac{u^2}{w_o^2}$$

where $w_o = 8.5$ (a constant)
 $u =$ wind speed (m/sec)

In the URI model, this quantity is modified by an exponential decay factor with a time constant of two days. This exponential decay of the volume of oil entrained was selected in an ad hoc fashion, as was the two day time constant, to compensate for the expected decreases in entrainment with time due to emulsification and other weathering properties which tend to solidify the slick.

The second section of the routine is used only in the preview mode. At the end of each step, the mass of oil represented by each entrained is calculated.

CALLED FROM: SURFES

SUBROUTINES CALLED: None

Important Local Variables:

WSP - mass of spilllet (metric tons).

BSP - time of start of spilllet (seconds).

DCN - time constant for the exponential decay of the entrainment rate currently set at 2 days (172800 seconds).

SEC - number of seconds in one day.

AO - constant for dispersion equation.

WO - wind constant for dispersion equation (m/sec).

AMT - percent entrained per second.

PERCEN - amount of oil entrained per time step (fraction).

DIF - ratio of amount entrained per step and total amount in water column at that step.

DCY - time decay factor given by $e^{-(\text{time} - \text{BSP}) / \text{DCN}}$

Subroutine ENTRN

This routine controls the injection of the oil droplets into the water column. Its flow chart is shown in Figure IV-15.

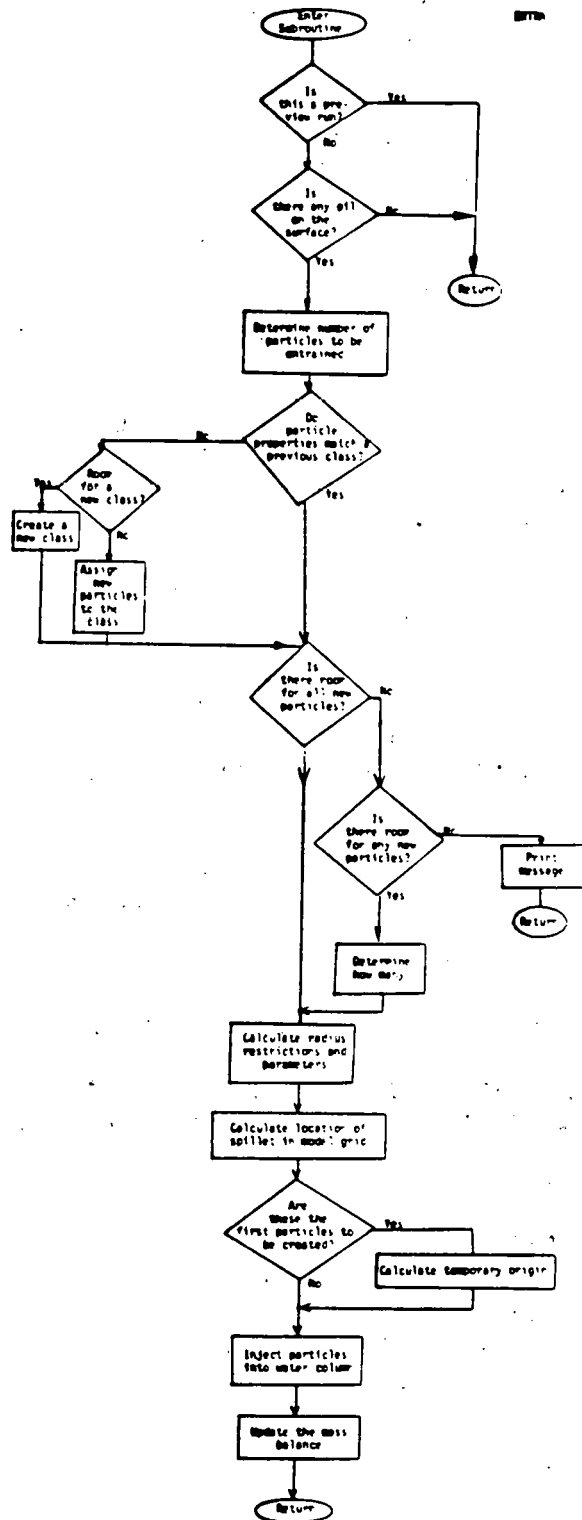


Figure 10 - 25. Flowchart of subroutine ENIN.

The first step is to determine from the input parameter, NRUN, whether or not this simulation is a preview. In the Preview mode, no particles are entrained. In the full simulation mode, the number of particles is determined according to the mass of oil entrained from the spilllet and the mass assigned to each particle. The particle properties are determined from the properties of the oil in the slick, which in turn determines the class to which the particle belongs. A maximum of 200 classes are currently allowed. The user may change this maximum by increasing or decreasing the input variables NTCLAS. If NTCLAS is increased, then array sizes in the common block PTP must also be increased.

The next step is to calculate the radius restrictions on the particle positions. These are determined in an ad hoc manner due to a lack of data regarding entrainment. The horizontal position is defined by a radial component and an angular component about the center of the spilllet. The angle, measured clockwise from the positive y axis is selected at random from a uniform distribution. The radial position is divided into two regions as defined by RLIM. For radii smaller than RLIM, the distribution increases linearly from zero. This coupled with the uniform distribution in angle gives an equal probability per unit area for particle location within RLIM. For radii larger than RLIM, the distribution decreases linearly to zero at RMAX. The maximum radius, RMAX, is a variable which decreases with the age of the spilllet. This procedure was adopted to provide sufficient extent to the subsurface distribution during the early time steps to avoid singularities in the diffusion equation, i.e., it is an ad hoc fashion of avoiding numerical instabilities in the early time history of the spilllet. A more elaborate procedure was not thought to be justified at this time because of our general ignorance regarding the entrainment process in general. In addition, there is certainly a thin surface sheen that spreads beyond the limits of our model prediction from which particles might be entrained.

The final step of the routine is to convert the polar coordinates of the entrained particle positions to model grid coordinates.

CALLED FROM: SURFES

SUBROUTINES CALLED: DIST, INJECT

Important Local Variables

RSPIL - spilllet radius

$$A = \frac{RO}{AFRAC^2} = \frac{RSPIL}{AFRAC^2} \text{ (RIFRAC)}$$

describes particle distribution within region one.

maximum radius for initial particle distribution.

$$D = \frac{(RO/A)^{1/2}}{RO} = \frac{RO * AFRAC^2}{RO} = AFRAC \quad \text{Temporary Variable}$$

$$B = \frac{(RMAX - RO)}{(1.0 - D)} = \frac{RMAX - RSPIL}{(1.0 - AFRAC) * RIFRAC} \quad \text{Temporary Variable}$$

$$C = \frac{(RO - RMAX + D)}{(1.0 - D)} = \frac{(RSPIL / RIFRAC - RMAX * AFRAC)}{(1.0 - AFRAC)} \quad \text{Temporary Variable}$$

XC, YC - position of center of spilllet with respect to depth grid origin in number of grid units from origin.

IX, IU, P - constants for random number generation used in subroutine Rand.

POMIN - minimum distance in x and y direction between the first two particles (meters).

RX, RY, RZ - random numbers between zero and one resulting from subroutine RAND.

RLIM - D - boundary of uniform distribution.

RADIUS - initial radial location of a droplet from the center of the spilllet.

- $A * RX^2$ - within RLIM
 - $B * RX + C$ - outside of RLIM

Also see Common Block INJC in Appendix III.

Subroutine EVPOR8

The mathematical formalism used in this subroutine is the same as that described by Wang, Yang, and Hwang (1976) but the numerical solution adopted in the present model is different. The equation to be solved for C_i , the average value of the percent weight of fraction i over the slick thickness, is:

$$d\bar{C}_i/dt = - \bar{D}_{ie} \bar{C}_i$$

where \bar{D}_{ie} is the average value of the evaporation diffusion coefficient over the slick thickness. The values of the diffusion coefficients are discussed in detail in the report of Wang et al. (1976) as well as in the

original paper by McKay and Matsugu (1973) and will not be further discussed here.

Wang et al. used the fourth-order Runge-Kutta method to determine \bar{C}_i . The difficulty with this method is that it requires storing all variables for two time steps. Because of the complexity of the model, use of the Runge-Kutta method resulted in a substantial requirement on computer memory. The following method was, therefore, adopted to determine $\bar{C}_i(t)$, given $\bar{C}_i(t - \Delta t)$ where Δt is the step size. The interval Δt was divided into N intervals of duration δt , i.e., $\Delta t = (N)(\delta t)$. The evaporation diffusion coefficient is assumed to be constant over each subinterval, although it may vary from one interval to the next. This then leads to:

$$\bar{C}_i(t) = C_i - (t - \Delta t) e^{-\left(\sum_{i=1}^n \bar{D}_{ie} (t - (j - 1/2) \delta t) \delta t \right)}$$

where $D_{ie}(t - (j - 1/2)\delta t)$ represents the value of D_{ie} at time $t - (j - 1/2)\delta t$. Solutions using this method were compared with solutions for the same input conditions using the model of Wang et al. (1976) and were found to differ by less than ten percent for $N=1$. The execution time was less by a factor of four and the memory requirements were significantly reduced (about twenty kilobytes).

The variable D_{ie} is defined by:

$$D_{ie} = km (P_i - P_{i\infty}) / (RT_S)$$

where P_i - hydrocarbon vapor pressure of fraction i at the interface.

$P_{i\infty}$ - hydrocarbon vapor pressure of fraction i at infinite altitude.

R - the gas constant.

T_S - the oil slick temperature.

and

$$km = \text{CONST} * e(Q \text{ WVEL}) * \text{AREAR}$$

where CONST, Q and R are constants defined within the routine,

WVEL - wind velocity in meters/sec.

A - area of spilllet in square meters.

See Figure IV-16 for a flow chart of this subroutine.

CALLED FROM: SURFES

SUBROUTINES CALLED: None

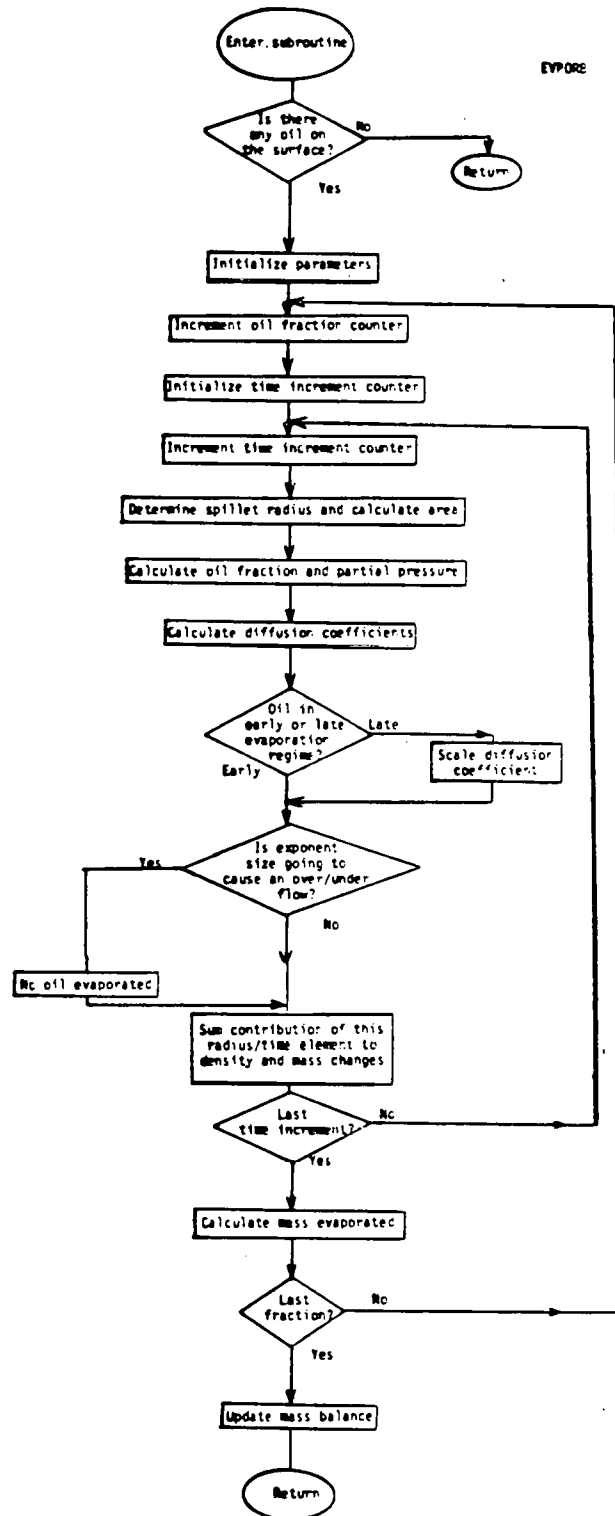


Figure IV.-16. Flow chart for subroutine EVPORE.

Important Local Variables:

ABSZERO absolute zero (degrees centigrade).
AREA area of spillet (meters²).
CON1, CON2 - array of constants for Antoinies equation of partial pressure.
DAGRES - average temperature over the slick (degrees centigrade).
RAD - radius of the spillet during the integration process
 (meters).
DELTA - time of the substep in the integration (sec).
NINT - number of steps in the integration procedure.
OLDRAD - radius of spillet at the last time step (meters).
P - vapor pressure.
Q,R,CONST - constants for diffusion coefficient.
RC - universal gas constant.

Subroutine GRIDEX

This subroutine (see Figure IV-17 for its flow chart) expands and translates the floating grid so as to incorporate all of the marker particles. It determines the maximum and minimum positions of the particles and creates a grid with a particle free region 1.5 grid units wide around the entire periphery. This is required by the interpolation technique. If any particles get too close to the edge of the fixed depth grid, the floating grid is moved away from the boundary and the particle is lost. This routine prints a description of the floating grid every NPRSUB steps. The print parameter, NPRSUB also determines whether or not the means and standard deviations of the particle locations are to be calculated and printed. These last values are not passed out of the subroutine.

CALLED FROM: SUBSUR, PRINT

SUBROUTINES CALLED: None

Important Local Variables: None

Subroutine INITSS

This subroutine (see Figure IV-18 for a flow chart), called by the main section, initializes all of the subsurface drift and diffusion variables and parameters. It also initializes the droplet properties and subsurface print parameters. (See INPUT parameter description).

CALLED FROM: Main

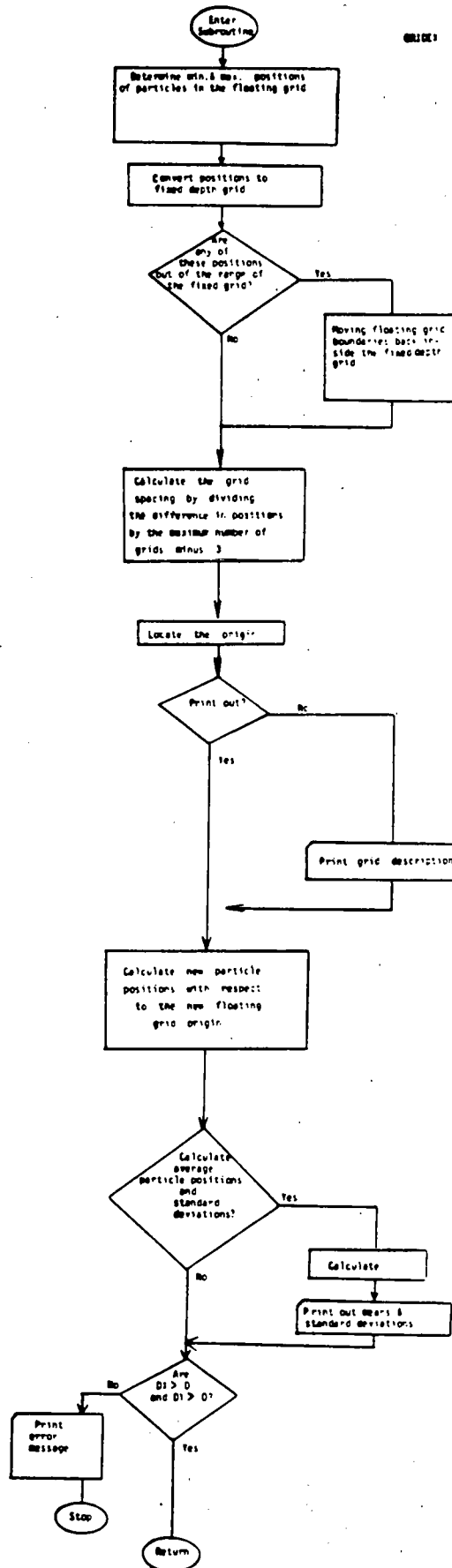


Figure 11-17 Flow Chart for subroutine GRID1.

INITSS

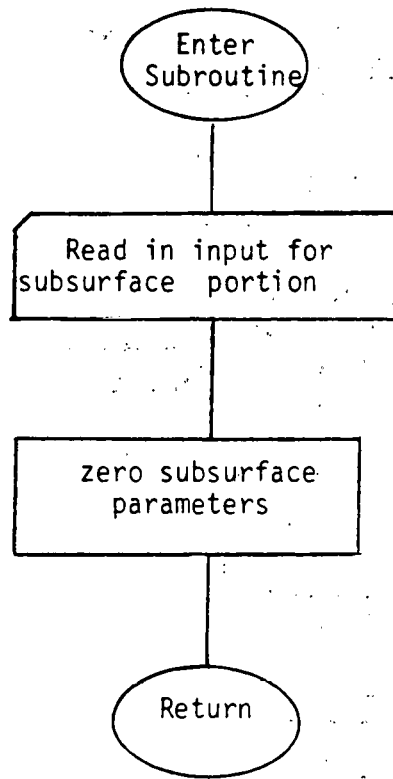


Figure IV.-18. Flow Chart for subroutine INITSS.

Subroutines called: READI, READF

Important local variables: None

Subroutine INJECT

This subroutine uses the radii restrictions calculated in ENTRN to determine the initial particle positions. A random number generator (see subroutine RAND) is used to obtain three dummy variables. The first one (RX) is used to determine the spacing of the marker particle from the center of the spilllet. The second random number (RY) is used to determine the random angle. The angle and radius determine the particles location in polar coordinates which is then converted to the rectangular grid. The particles location in the model grid undergoes two tests. First, the particle must be within the fixed grid. Second, if this is the first step, the first two particles created must have a separation that exceeds the input variable POMIN. This insures that a floating grid can be created in both directions. A third random number is used to determine the particle's position in the vertical which on the average is located at the depth by the input variable DEPC. See Figure IV-19 for a flow chart of the subroutine.

CALLED FROM: ENTRN

SUBROUTINES CALLED: RAND

Important Local Variables: see ENTRN for a description of variables used in inject.

Subroutine LOC8

This subroutine, flowcharted in Figure IV-20, determines the smallest rectangle of fixed grid elements that contains a spilllet. It is used to determine for which grid nodes the values of the specified environmental variable must be averaged. All nodal values falling on the edge of and within the rectangle completely containing the spilllet are used. These values are averaged and returned to the calling routine. If the fixed grid consists of only one value, that value is used. If the spilllet lies completely outside of the specified fixed grid, a message is written and the control parameter MDLSPL is changed from 0 to 1. If this condition arises, none of the surface processes will be executed on return to the calling routine except for shoreline interaction if, indeed, the spill has hit the shore.

CALLED FROM: SURFES

SUBROUTINES CALLED: DIST

Important Local Variables:

- MDLSPL - 0 if the spilllet is in the study area.
- 1 if the spilllet is outside one of the environmental grids.
- NGRO - number of grids that define a variable.

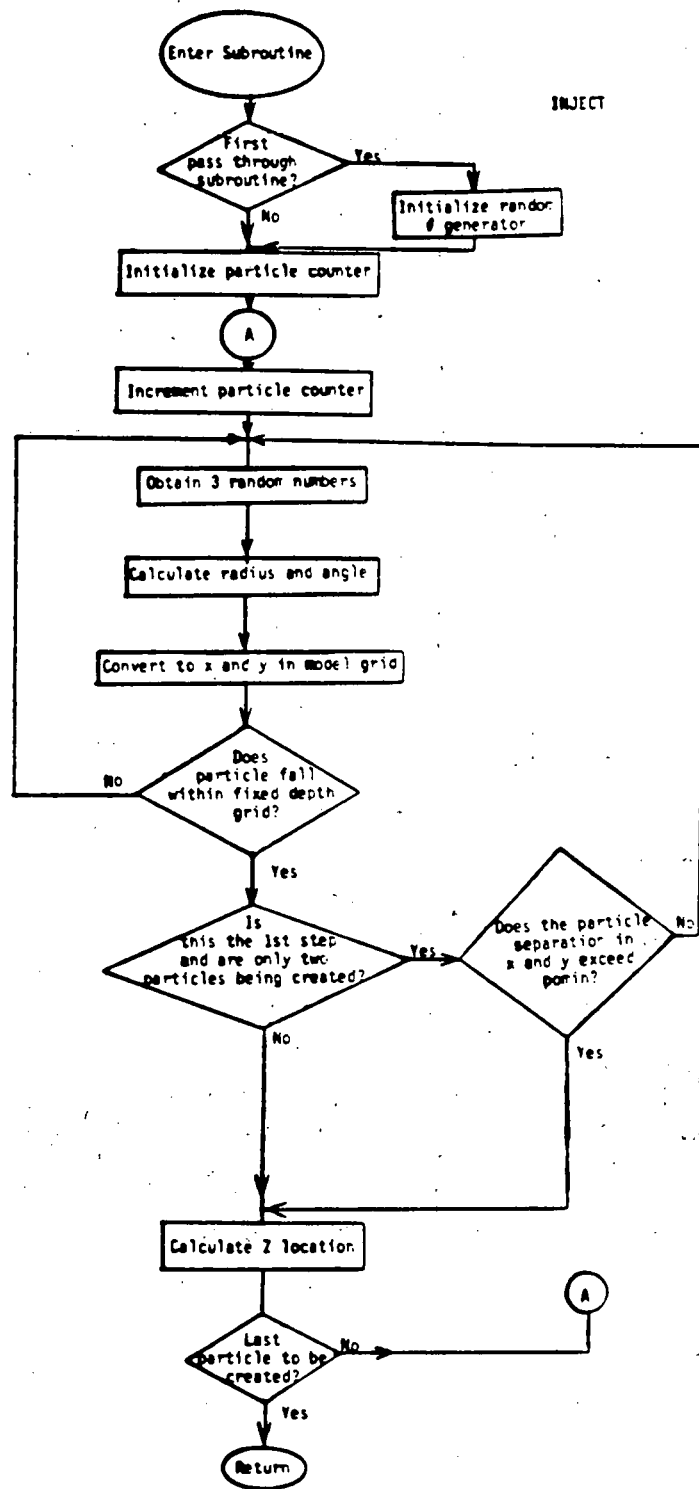


Figure IV - 19. Flowchart for subroutine INJECT.

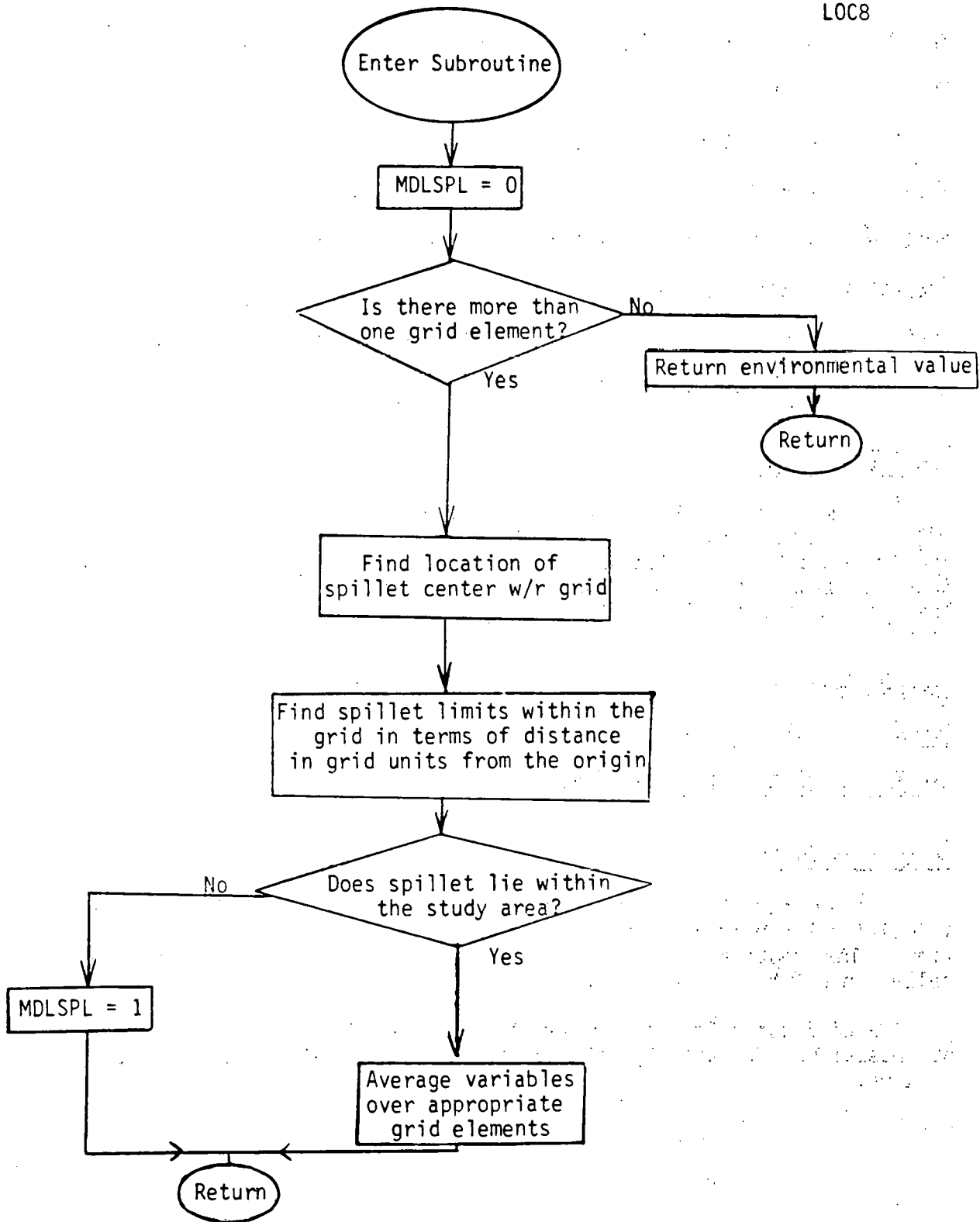


Figure IV - 20. Flowchart for subroutine LOC8.

- NX, NY - maximum number of grids in X and Y direction.
- ANG - angle between x axis and lines of constant latitude.
- XL, YL - Longitude and Latitude of (1,1) grid position.
- XS,YS - grid spacing in X and Y direction (meters or degrees).
- VAR1,VAR2, - input arrays, if NGRD is 1, VAR2 is not used.
- VAL1,VAL2 - averaged values of the above arrays.
- XC,YC - Longitude and Latitude of the center of the spilllet.
- R - spilllet radius (meters).

Subroutine MASSC

This subroutine, flowcharted in Figure IV-21, calculates and writes the mass balance both in terms of the total amount of oil in each region and the percentage of oil in each region. In addition to the mass balance, it also writes out statistics on the number of particles present, lost or deposited. The mass data may be written to disk and/or the line printer.

CALLED FROM: Main

SUBROUTINES CALLED: None

Important Local Variables: None

Subroutine PARTV

This subroutine uses the bilinear weighting scheme to interpolate the velocities known at the floating grid nodes to the marker particle position. The routine is flowcharted in Figure IV-22. The subroutine is called once for each particle.

The bilinear weighting scheme obtains the value of a variable located at positions f_x and f_y in a grid element, see Figure IV-23, as follows:

$$U = (U_1 + f_x (U_2 - U_1)) + f_y ((U_1 + f_x (U_2 - U_1) - (U_3 + f_x (U_4 - U_3)))$$

where U is the value sought and all other values are defined in Figure IV-22.

CALLED FROM:

SUBROUTINES CALLED: None

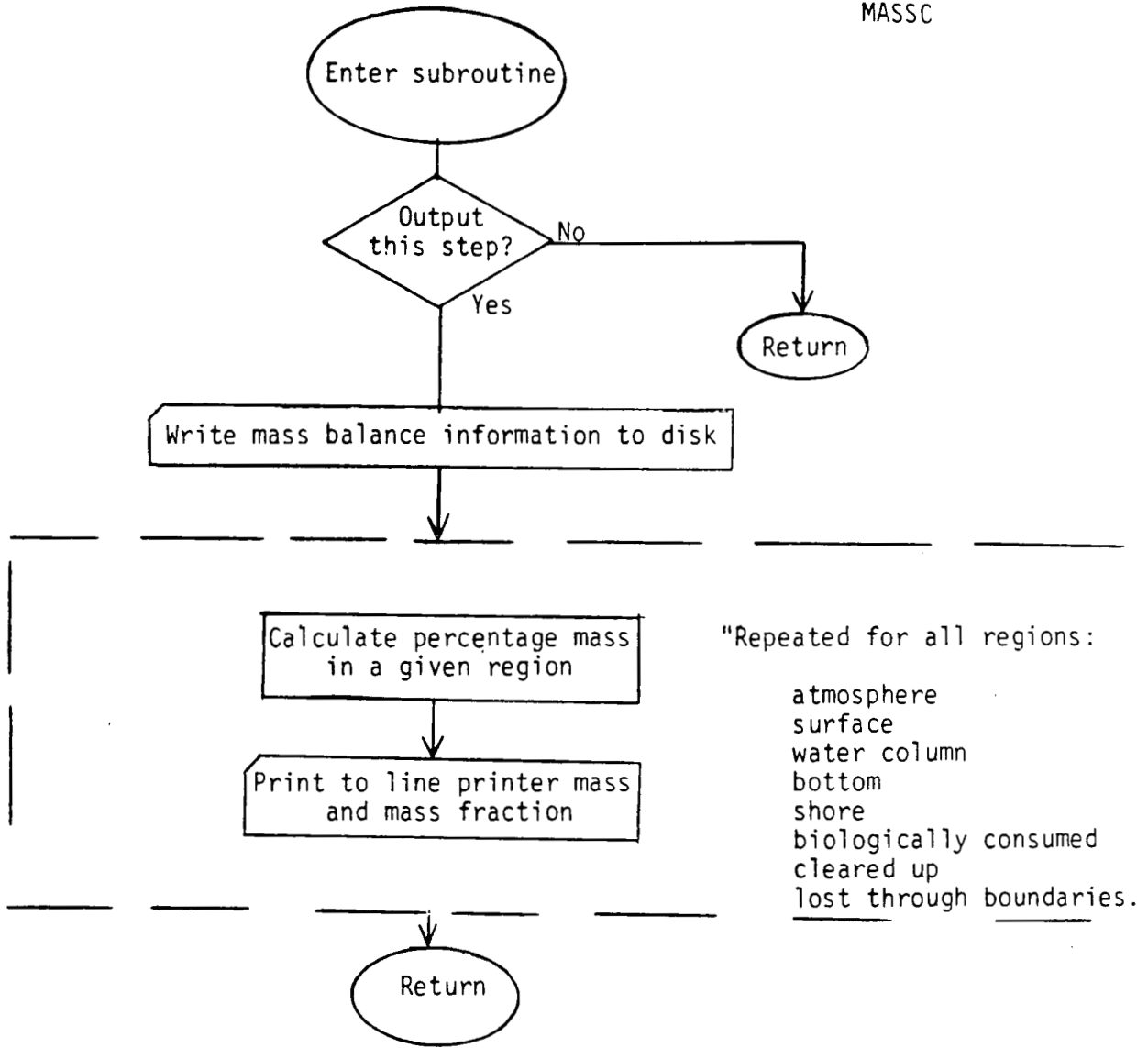


Figure IV - 21. Flowchart for subroutine MASSC.

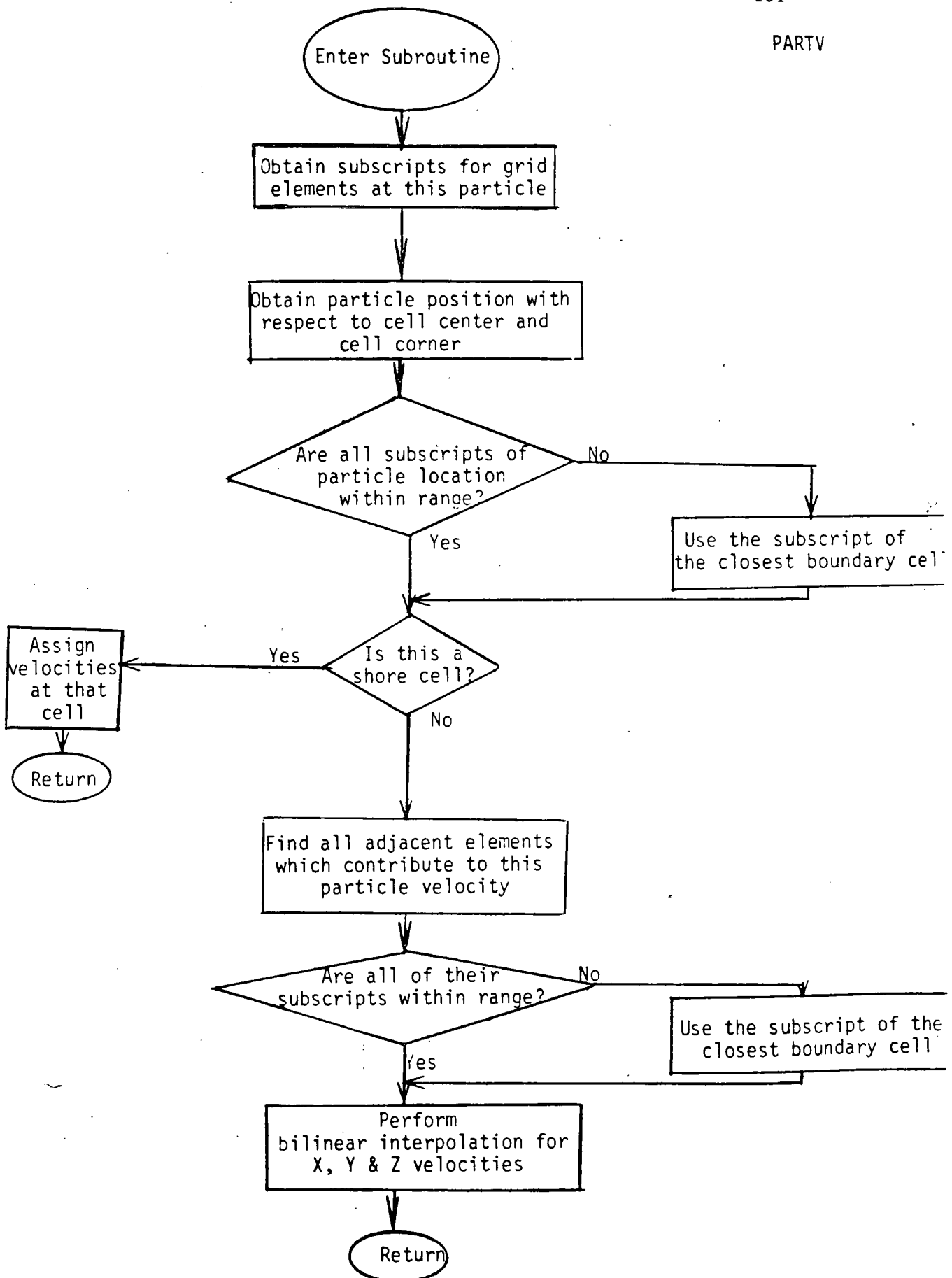


Figure IV - 22. Flowchart for subroutine PARTV.

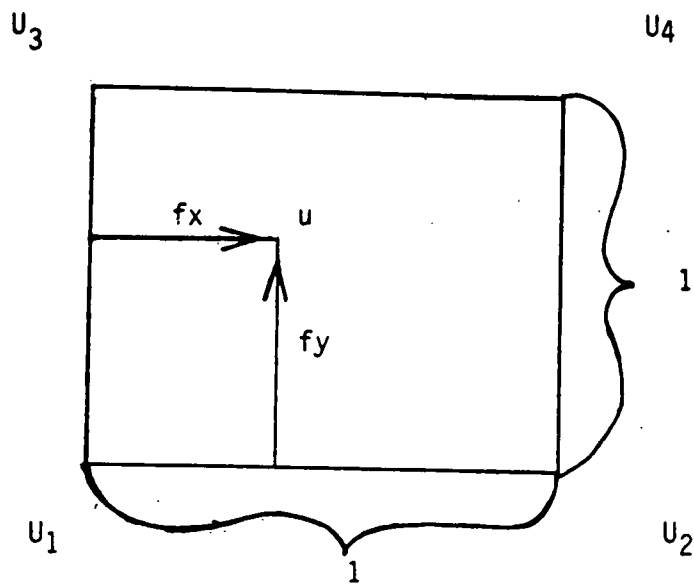


Figure IV. - 23. Defining figure for Bilinear interpolation scheme.

Important Local Variables: None

Subroutine PRINT

This subroutine handles most of the output operations for the sub-surface section of the model. The output is controlled by print control parameters described in common block PRINT. These parameters control both the paper and the disk output. The subroutine will print out the velocity field and the concentration matrix on the floating grid with headers locating the floating grid with respect to the origin of the fixed depth grid (in meters or degrees). In addition, the actual location of each marker particle can be printed if desired. When printing these positions, the depth is calculated and printed in meters if a z transformation is being used in the simulation. Printout is controlled by KPRTV, KPRTC and KPRTP for the velocity and concentration grids and the particle positions, the value of these control parameters specifies the step interval between printing. If the parameter is equal to zero, no printout for the corresponding variable is generated.

Output to disk is controlled first by the parameter NPRD. If it is zero, subroutine PRINT will output nothing to disk. If NPRD equals 1, then the parameters NPRV, NPRC, and NPRP define the step interval at which the various data sets are to be output.

A flow chart of this subroutine is shown in Figure IV-24.

CALLED FROM: SUBSUR

SUBROUTINES CALLED: BOUNV, CONC, GRIDEX

Important Local Variables:

- NCALL1 - flag so as not to call the subroutine CONC twice.
 - 0 call CONC the second time it is encountered.
 - 1 call CONC only during the first concentration printout.
- RIO(IMSUB) - 15 - X positions of the floating grid cells (meters or degrees).
- RJO(IMSUB) - 15 - Y positions of the floating grid cells (meters or degrees).
- XTEMP, YTEMP, ZTEMP - particle positions with respect to the fixed depth grid (degrees or meters).

Subroutine RAND

This routine generates random numbers from a uniform distribution between 0.0 and 1.0. The input variables to this routine are all initialized in subroutine INJECT.

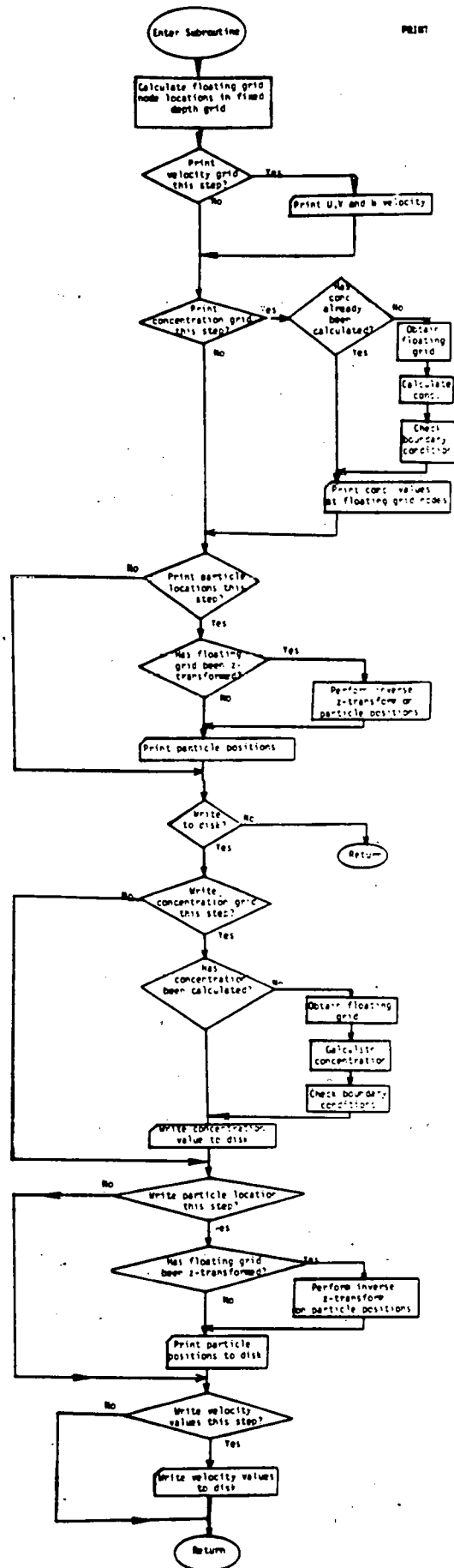


Figure 11 - 24. Flowchart for subroutine PRINT.

CALLLED FROM: INJECT

SUBROUTINES CALLED: None

Important Local Variables: None

Subroutine READI

This subroutine, flowcharted in Figure IV-25, is used to input, and check to some degree, all scalar integer variables. The required input format is described in Appendix I. The subroutine reads the value of the variable and the variable name. If the variable name that it reads does not agree with the name of the variable passed to it from the calling routine, an error message is written and execution of the program terminates. This prevents reading cards out of order. In addition, if the value of the variable does not lie in some predefined range again passed to it from the calling routine, an error message is written and execution terminates. This is to help avoid exceeding the limits of various arrays as well as reducing the chance of an abnormally long run resulting from the improper positioning of the input parameter. If the upper and lower limits specified in the call to READI are equal, any value may be entered.

CALLLED FROM: MAIN, INITSS

SUBROUTINE CALLED: NONE

Important Local Variables:

- I - value read from input and passed back to the main program.
- NL - lowest value permitted.
- NU - greatest value permitted.
- XNAME - name of variable to be read.
- XPNAME - name of variable read from input stream.

Subroutine READF

This subroutine is used to input, and to check to some degree, all single real variables. It is identical to READI except that:

1. It reads floating point numbers rather than integers.
2. There are no restrictions on the range of the number read in other than those of the computer.

Subroutines called: None

CALLLED FROM: MAIN, INITSS

READI

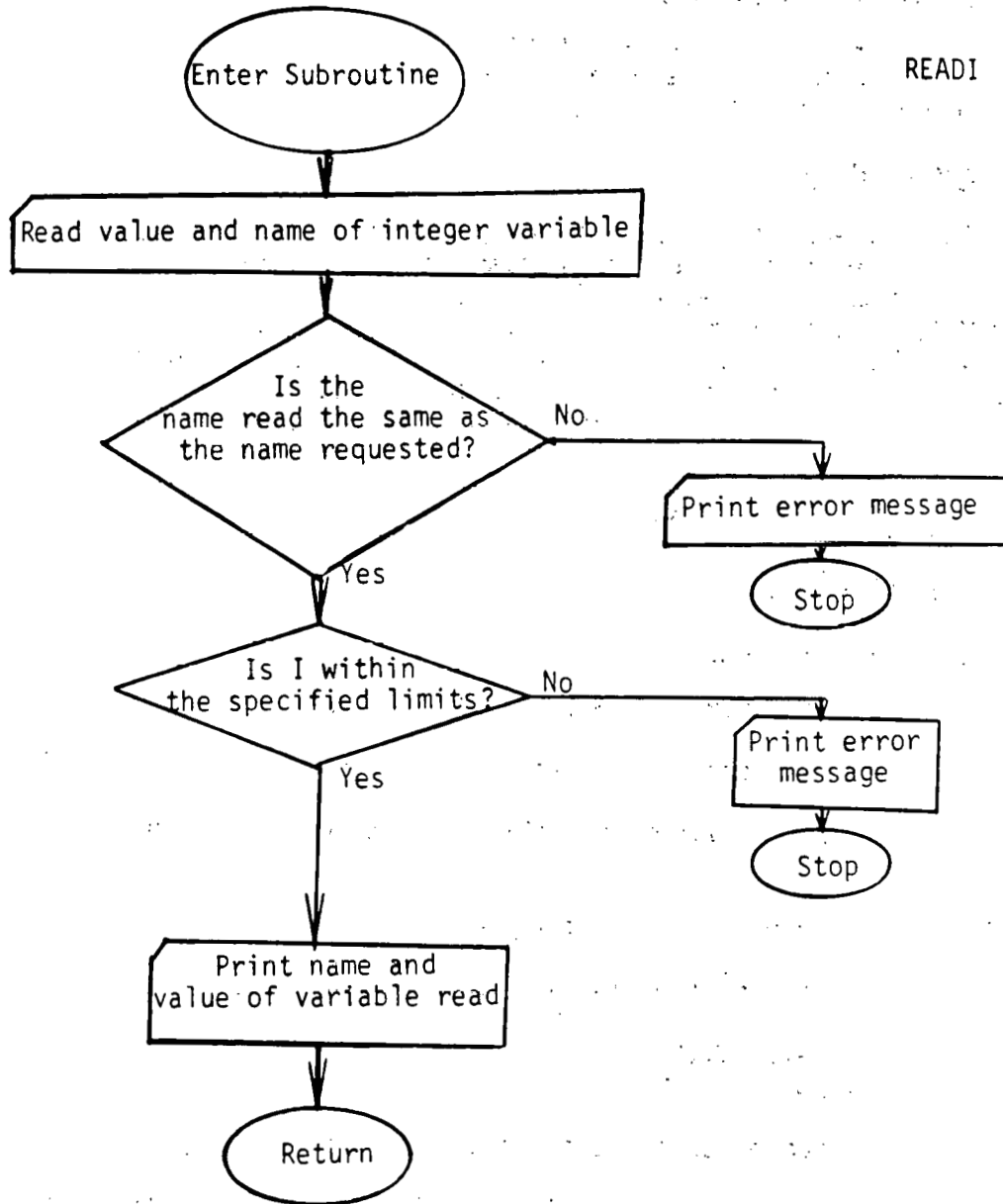


Figure IV - 25. Flowchart for subroutine READI.

Important Local Variables:

- X - value of variables read in and passed to the calling routine.
- XNAME - name of the variable to be read.
- XPNAME - name of the variable read from the input stream.

Subroutine REMOV

Each cleanup and treatment effort initiated has associated with it a duration. When this length of time has been exceeded, the effort is to be terminated and removed from the list of cleanup/treatment efforts. REMOV is used to remove an expired effort from the list (see Figure IV-26 for its flow chart). The routine removes an effort by simply moving the last effort on the list into the location occupied by the expired effort and then decrements the counter specifying the number of active efforts by one.

CALLED FROM: CLNUP, TREAT

SUBROUTINES CALLED: None

Important Local Variables:

- BEG - beginning of this effort (hour).
- DUR - duration of this effort (hours).
- DUM - dummy variable which is equivalenced in the Subroutines TREAT and CLNUP.
- MEM - number of current efforts.
- NVAR - length of variables in the common bloc.
 - 7-for CLEN
 - 10-for CHEM
- JTEMP - number of expired efforts this step.
- MTEMP - last efforts on list; this one is moved to expired efforts placed in list
- LTEMP - effort which has expired and is being replaced.

Subroutine ROTAT

This subroutine, flowcharted in Figure IV-27, converts locations from the fixed depth grid to any of the environmental grids. It is used primarily to map values of environmental variables into the floating grid. The depth grid is used as the reference because the floating grid is defined with respect to it. The output of this routine is the x and y location of the point of interest referred to the new environmental grid.

CALLED FROM: BOUNV, VELC

SUBROUTINE CALLED: DIST

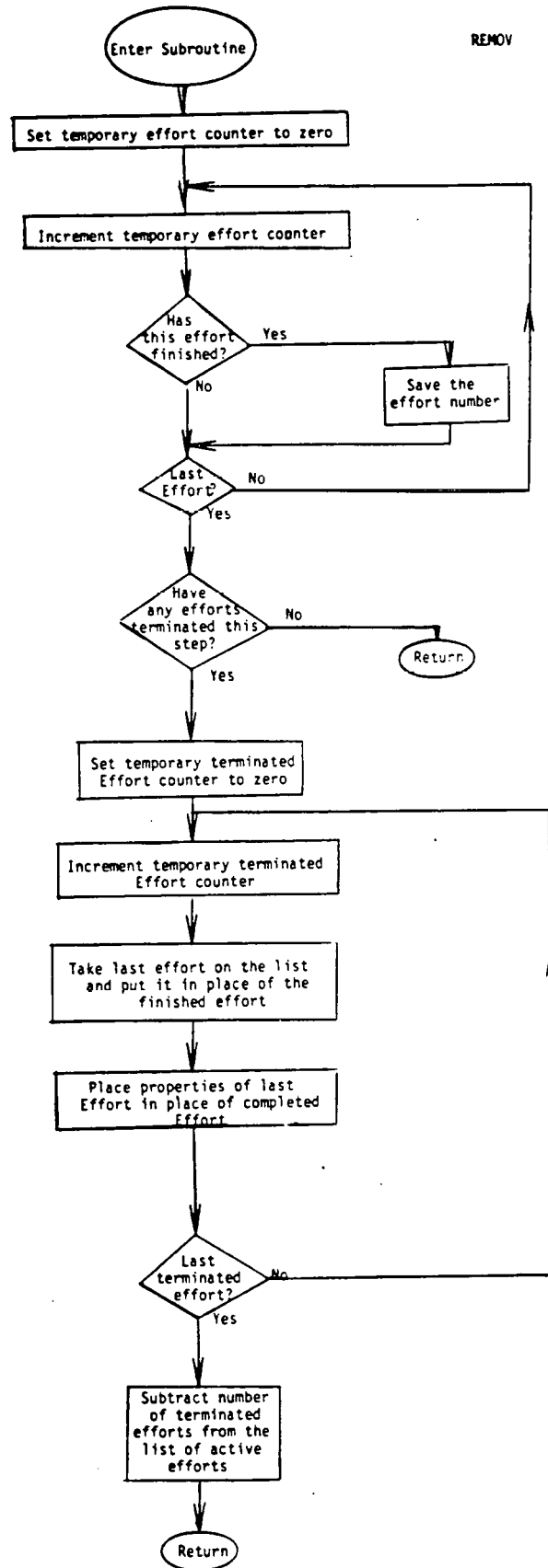


Figure. IV. - 26. Flowchart for subroutine REMOV.

ROTAT

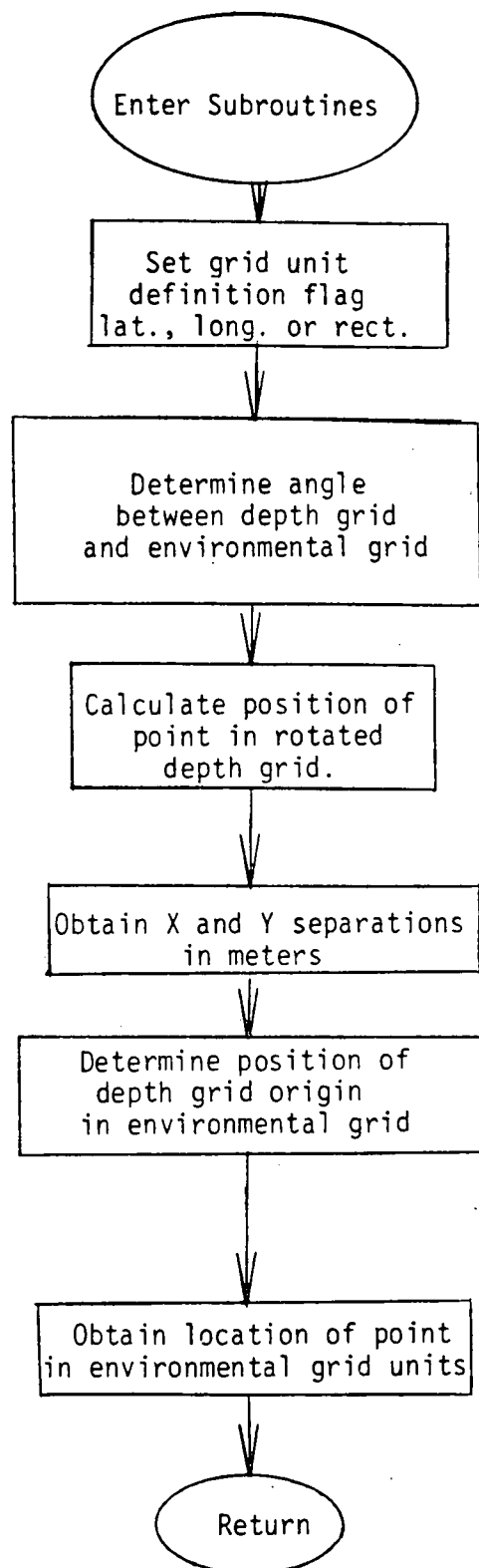


Figure IV. - 27. Flowchart of subroutine ROTAT.

Important Local Variables:

- XL,Y1 - longitude and latitude of the (1,1) location of the grid of interest.
- XD,YD - grid spacing in X and Y direction for the grid of interest (meters or degrees).
- ANG - angle of X axis with lines of constant latitude for the grid of interest.
- XD,YD - position of point which is to be converted. This is with respect to the depth grid.
- XG,YG - grid position of point with respect to the grid of interest.
- XSP,YSP - distance between origins of depth grid and grid of interest.

Subroutine SHORE

This subroutine reads the longitude and latitude values of the points defining the shoreline. The subroutine is always called but if the study area includes no shoreline, then no points are read.

CALLED FROM: MAIN

SUBROUTINE CALLED: None

Important Local Variables: None

Subroutine SPILIN

This subroutine reads in all new spilllet parameters and initializes any properties not read in. The user is referred to Appendix IX for general oil properties. The routine will also print all current spilllet information at the step interval specified by the parameter NSPPRP (see input variables). Spillet information may also be written to a disk data set at a step interval defined by the parameter NSPPRD. Finally, a section is included in the routine for restart runs. It reads in old spilllet information and skips the initialization which have already been performed (see Figure IV-28 for a flow chart of the subroutine).

CALLED FROM: MAIN

SUBROUTINES CALLED: None

Important Local Variables: None

Subroutine SPREAD

The spreading process is described by the simple three regime spreading mechanism proposed by Fay (1969). The only peculiarity in this model

SPILIN

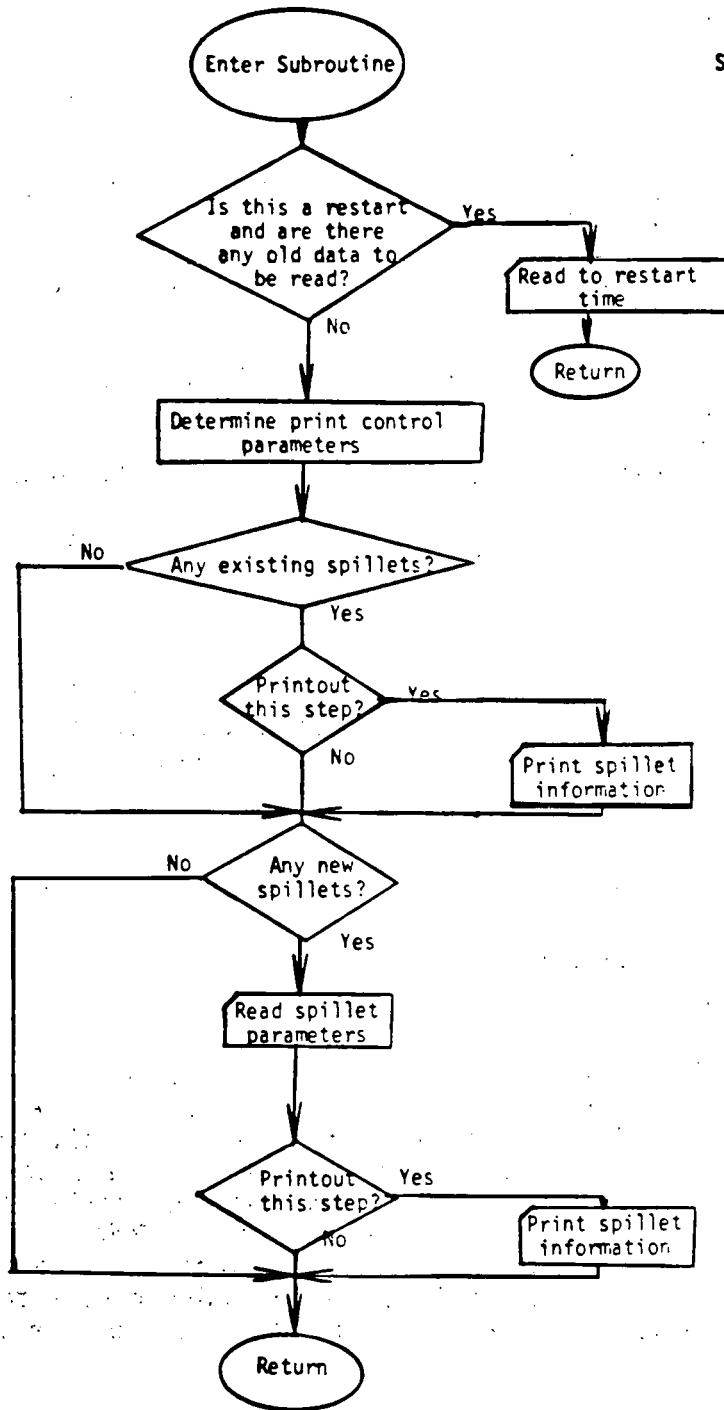


Figure IV. - 28. Flowchart for subroutine SPILIN.

with regard to spreading is the fashion in which the time, t , used in the various equations for the radius is determined. In this model, a fictitious time is determined by solving each of the three different regime radius equations for time using the value of the radius from the previous step and the volume of spilled oil remaining at this time step. From these three values of "time," the appropriate regime is determined. Then the derived value of time is incremented by the time step of the model and the new radius is calculated. For a simple spill with no new oil added or oil previously in the slick removed, this yields the same value of radius with time as the original Fay formulation. However, for the case where oil is removed or added, this allows for the rate of spreading to jump from one regime to another. It is obvious that this is necessary if one considers a slick in the third regime which is treated with a chemical dispersant which lowers the spreading tension, by an order of magnitude. In this case, without changing the "time" variable used in the spreading equation, the radius changes by a factor of three. Equally drastic changes would result from the removal or addition of oil by any of the means available in the model. It is as a result of this regime changing mechanism that Fay's spreading formalism is used rather than the combined spreading-horizontal diffusion mechanism used in some of the more recent models (Wang, Campbell and Ditmars, 1975). See the flow chart in Figure IV-29.

CALLED FROM: SURFES

SUBROUTINES CALLED: None

Important Local Variables:

COEF1 - spreading coefficient for first regime.
COEF2 - spreading coefficient for second regime.
COEF3 - spreading coefficient for third regime.
DELTA - (water density - oil density)/water density.
GRAV - gravitational acceleration (cm/sec**2).
RAD - radius of spillet (cm).
RHOW - density of sea water (gm/cc).
RMAX - maximum radius for a spillet containing a given volume of oil.
SIG - spreading tension (dynes/cm = gm/sec**2).
T_{ij} - time at which spillet goes from Regime i to Regime j.
VISHZO - viscosity of sea water (stokes = cm**2/sec).
VISRTZ - square root of VISHZO.
VMIN - maximum volume for which Fay's Regime 2 is skipped.

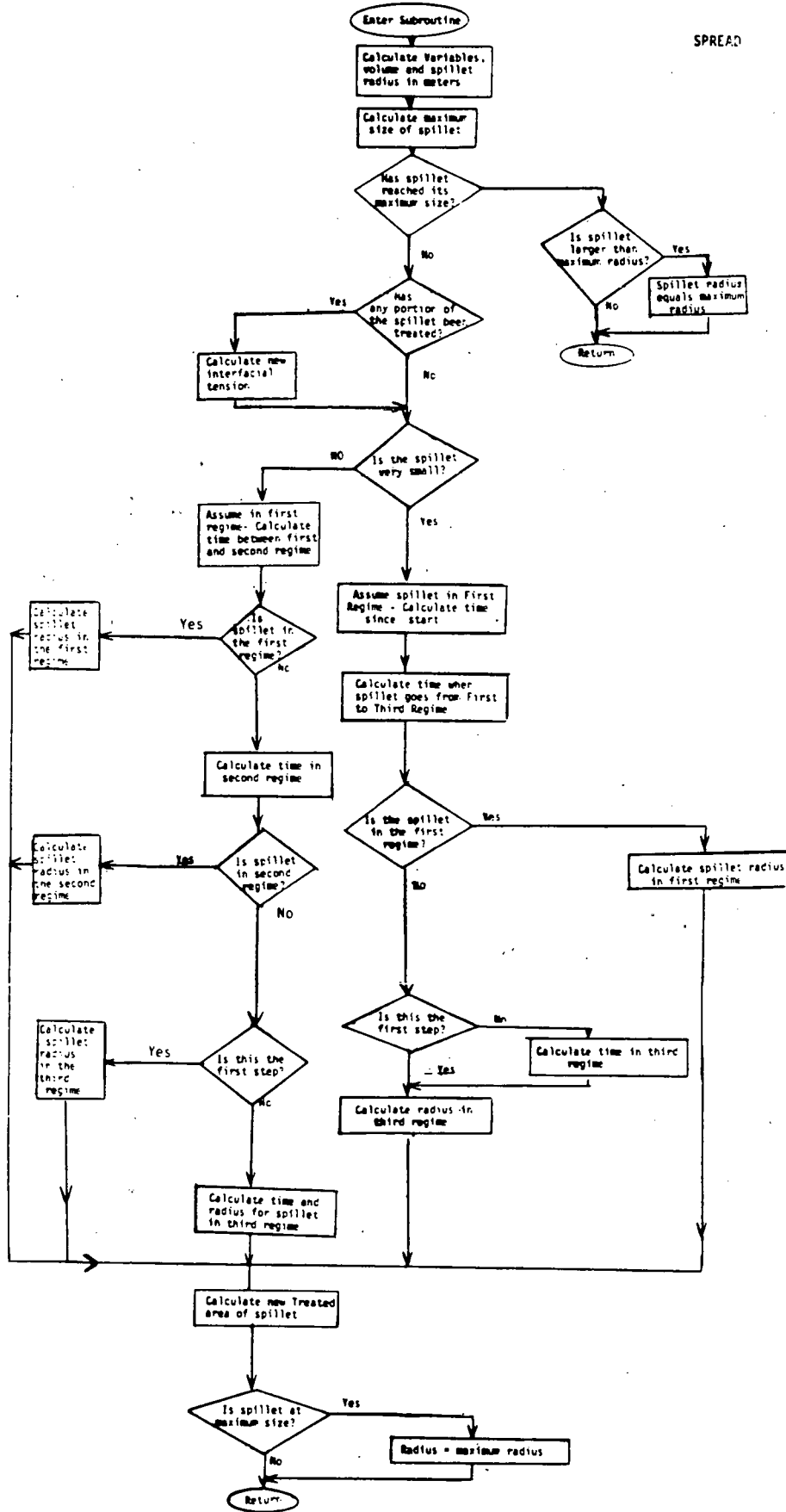


Figure IV. - 29. Flowchart for Subroutine SPREAD

VOL - volume of spilled oil (cc).

Subroutine SUBSUR

This subroutine calls the seven main subroutines which advect and diffuse the subsurface droplets in the water column. The method is based on the Water-Advective-Particle-In-Cell method developed by Pavish and Spaulding (1976-1977). A brief overview of the numerical scheme, along with a discussion of those factors which have been modified specifically for this application, is presented below.

The three-dimensional mass transport equation is solved using a particle-in-cell method. This is a quasi Monte Carlo technique in which representative particles are sampled at random from a predetermined distribution. The space which these "marker" particles occupy is then divided into a number of rectangular cells. The concentration distribution of the particles is determined by calculating the number of particles in each cell, i.e., this yields the concentration at the center of that cell. The model then obtains the concentration gradient and calculates the resulting diffusive velocity, which it adds to the advective velocity input to the program, to obtain the total particle velocity. Finally, the particle velocity is used to move the individual particles.

The fundamental equation being solved is the transport diffusion equation:

$$\frac{\partial C}{\partial t} + \vec{U}_A \cdot \vec{\nabla} C = \vec{\nabla} \cdot k_{ij} \vec{\nabla} C + S_i$$

where C is the concentration of oil droplets,

k_{ij} is the diffusivity tensor,

\vec{U}_A is the advection velocity assuming incompressibility, and

S represents either a source or sink of oil.

This equation may be rewritten in the advective-diffusion form:

$$\frac{\partial C}{\partial t} + \vec{\nabla} \cdot (C \vec{U}_T) = 0$$

where

$$\vec{U}_T = \vec{U}_A + \vec{U}_D$$

\vec{U}_T - Total particle velocity

\vec{U}_A - Advective velocity

and

\vec{U}_D - Diffusion velocity, defined by

$$\vec{U}_D = - \frac{k_{ij}}{C} \vec{\nabla} C$$

The total particle velocity is solved using a finite difference representation on the space staggered grid shown in Figure IV-30.

This sophisticated subsurface drift model was selected for several reasons, the main one being that it allows for oil droplets of varying properties, for example some denser than water that may sink and some less denser than water that may resurface as well as neutrally buoyant drops to represent the dissolved portion of the spill. In addition, the chemical properties of the droplets may vary, and this variability may be a function of particle size.

Another important feature of the subsurface portion of the model is the mixed Eulerian-Lagrangian coordinate system. The Eulerian coordinate system is the one on which the tidal currents, the bathymetry and the computational cells are defined. The Lagrangian coordinate system is the one on which the oil droplet concentration is defined. This system expands and translates so as to always include all particles. Variables defined on the Eulerian system are interpolated to the Lagrangian system. The Lagrangian system also allows for a coordinate transformation on z, the vertical variable, such that the water column at every horizontal node is divided into the same number of equally spaced layers. This means that as the water becomes shallower, the vertical grid spacing becomes smaller, thus keeping the same relative vertical resolution.

The flow of this routine, Figure IV-31, is quite straightforward.

CALLED FROM: MAIN

SUBROUTINES CALLED: BOUNV, CONC, COURAN, DISPV, GRIDEX, PRINT, VELCT

Important local variables:

C(IMSUB, JMSUB, KMSUB)	15,15,10 - oil concentration on the floating grid (mg of oil/ml of water).
M(IMSUB, JMSUB, KMSUB)	15,15,10 - computational cell definitions of the floating grid.
NST	step number.
HFLT(IMSUB, JMSUB, KMSUB)	15,15,10 - tidal elevations at the floating grid nodes (meters).
DFLT(IMSUB, JMSUB, KMSUB)	15,15,10 - depths at the floating grid nodes (meters).
CC(IMSUB, JMSUB)	15,15 - concentration values averaged over the water column.
NPTFLT	interval print control for subsurface information.

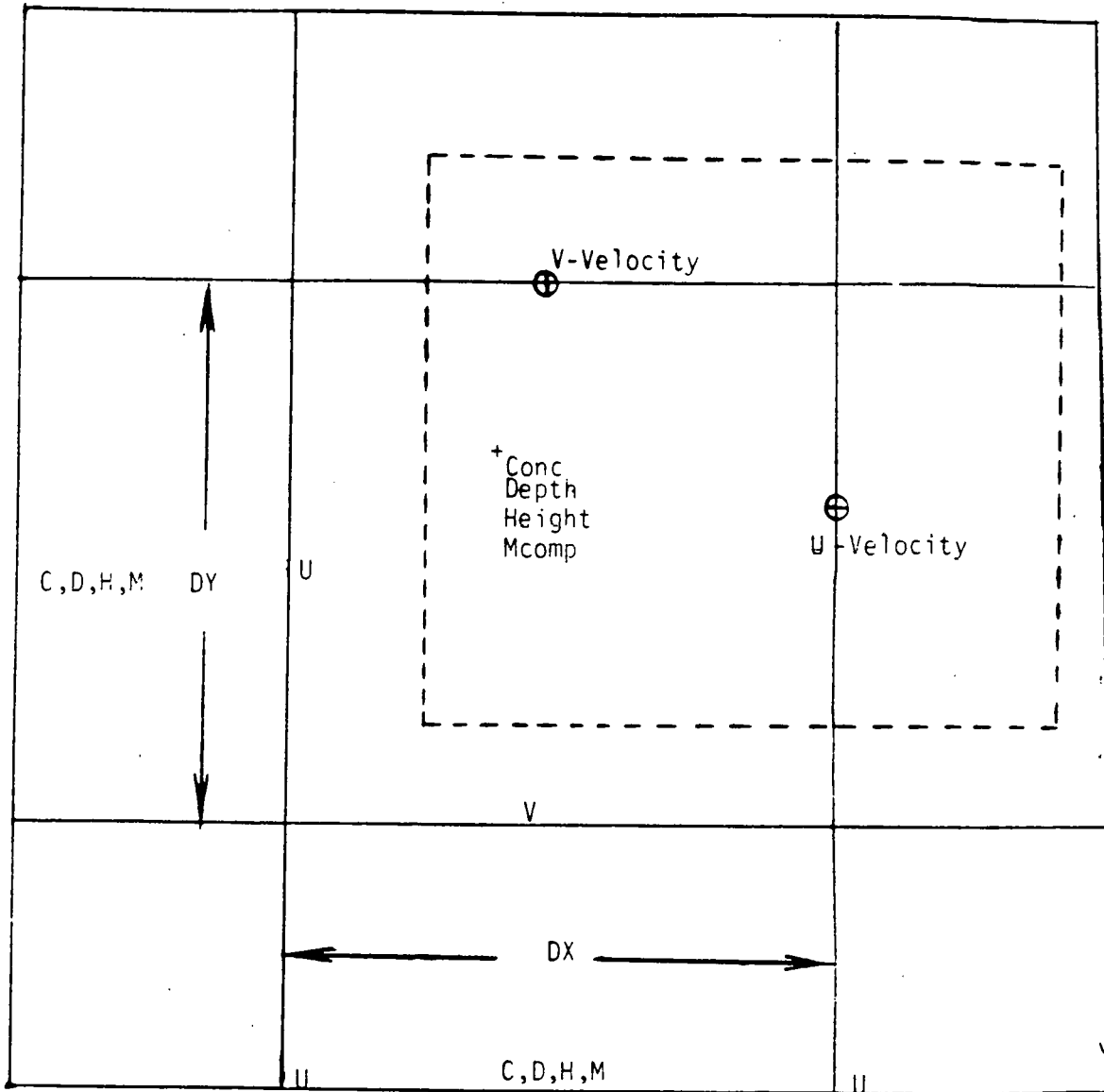
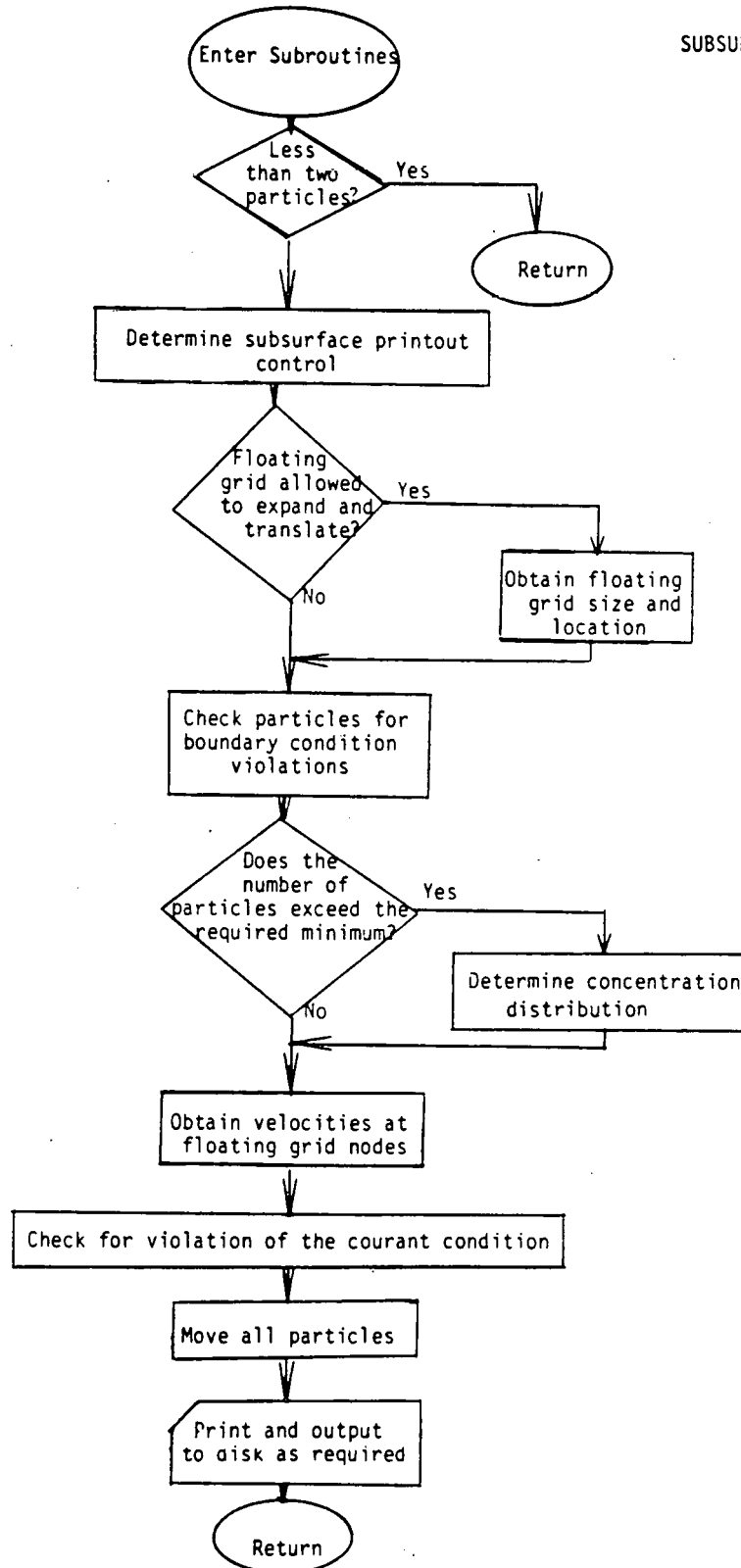


Figure IV-30. Space Staggered System
(Values Inside of Square have the same Indices)

SUBSUR



Figures IV.-31. Flowchart for subroutine SUBSUR.

NPTSUB

print control parameter as determined by NPTFLT

printout this step, 0 - no printout this step.

1 - printout this step.

Subroutine SUMMUP

This subroutine, flowcharted in Figure IV-32, writes to disk all of the variables describing the disposition of the spilled oil (the Restart data set). It also outputs active cleanup and treatment efforts. The subroutine is called at a step interval defined by the input parameter NSUMM, as well as at the end of the run. It codes the output with the step number. If the user wishes to restart the run from this point, new input and output data sets are to be used if NSTFN is set equal to zero (by the user). The reason for outputting the parameters outlined above is to allow the run to be restarted following its termination. Because the restart data set is overwritten everytime, SUMMUP is called, the run may be restarted only from the step at which the parameters were last written.

CALLED FROM: MAIN

SUBROUTINES CALLED: None

Important Local Variables: None

Subroutine SURDFT

This subroutine, outlined in Figure IV-33, is used to advect the surface portion of the oil spill, specifically, the spilletts. The advective velocity is taken equal to the vector sum of the ocean velocity, input to the model, and a scaler constant times the wind velocity, also input to the model. The scaler factor multiplying the wind velocity, WINFC, is presently set to .035 in the model and can only be changed by modifying the appropriate data statement. If the ocean current is in degrees/second, it will be converted in the subroutine to meters/second.

CALLED FROM: SURFES

SUBROUTINES CALLED: None

Important Local Variables

UCRNT - water current in x direction passed to the routine.

UWIND - wind speed in x direction passed to the routine.

VCRNT - water current in y direction passed to the routine.

VWIND - wind speed in y direction passed to the routine.

WINFC - wind factor defined in the routine.

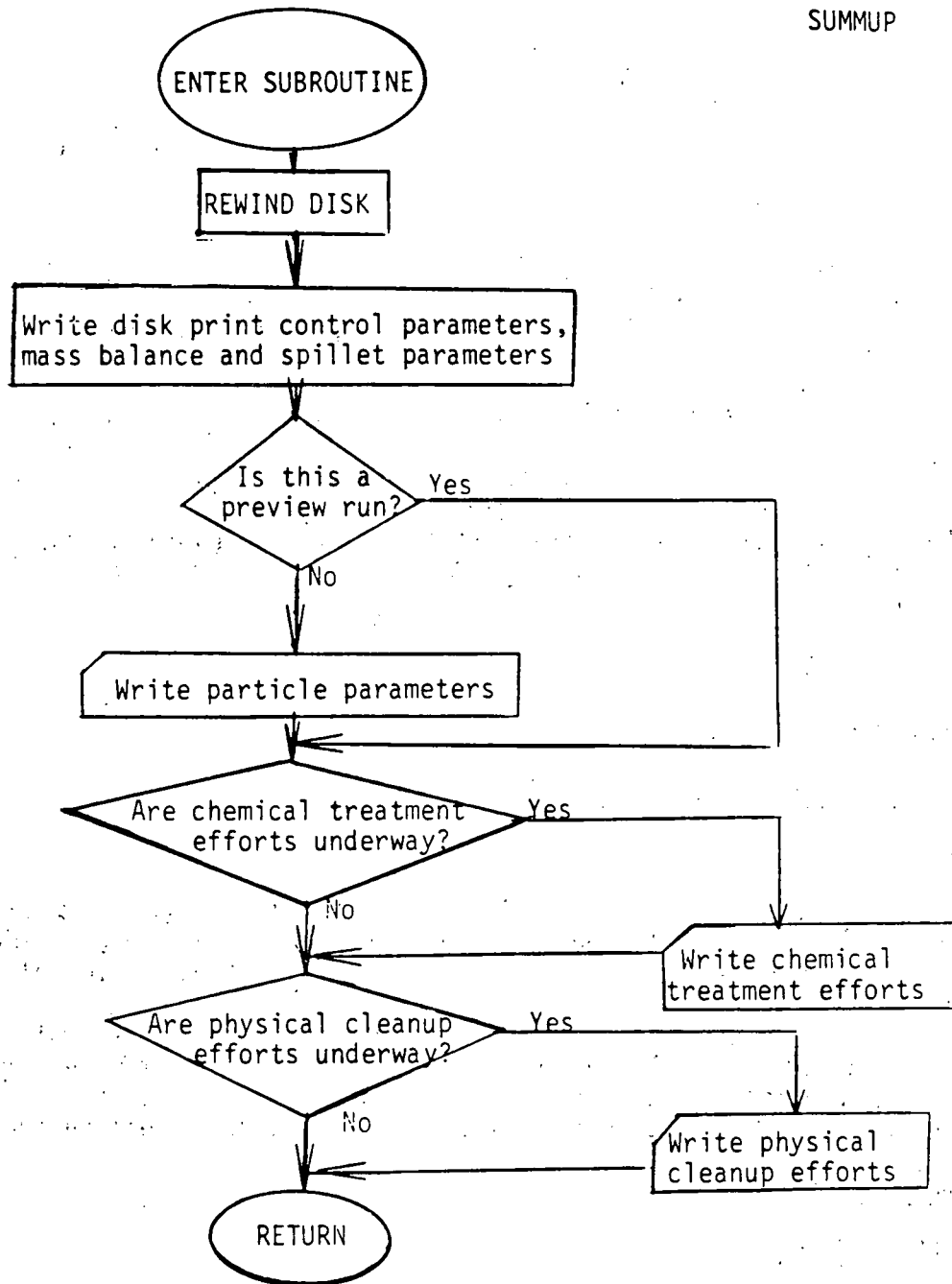


Figure IV. - 32. Flowchart for subroutine SUMMUP.

SURDFT

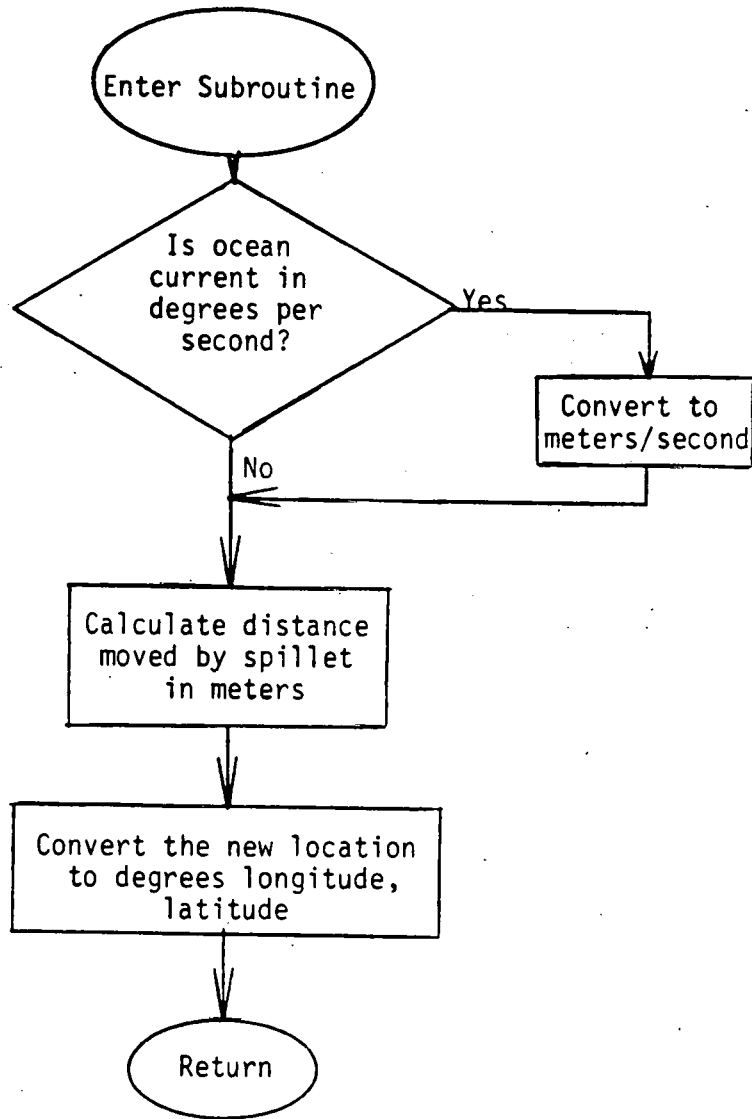


Figure IV. - 33. Flowchart for subroutine SURDFT.

Subroutine SURFES

The simulation model might be viewed as consisting of four major sections: the main program; the input module; the surface module, and; the subsurface module. Each of the last three sections consist of a number of subroutines. The subroutine, SURFES, controls the surface section, calling all of the subroutines that effect the disposition of the surface slick. With the exception of the shoreline interaction process, all processes are treated separately for each spillet, i.e., the subroutine representing a process is called once for each spillet. The flow through this subroutine (see Figure IV-34 for flow chart) is quite straightforward.

CALLED FROM: MAIN

SUBROUTINES CALLED: ASHOR, CLNUP, ENTMAS, ENTRN, EVPOR8, LOC8, SPREAD, SURDFT, TREAT

Important Local Variables:

- SUMAS - Amount of mass entering the water column from one spillet during one step.
- MDLSPL(NSPIL) - 99 - 0 - spillet is within study area.
1 - spillet is at edge of study area. This spillet is no longer subject to any processes.
- MDLSPL - Parameter in subroutine LOC8 which indicates whether or not the spillet is in the study area.
 - 0 - within study area
 - 1 - out of study area
- ENMAS - Mass of oil entrained this step. This is used in the preview run to determine the amount of mass to be represented by each droplet.
- UCRNT - Average current over spillet in X direction (m/sec or deg/sec).
- VCRNT - Average current over spillet in Y direction (m/sec or deg/sec).
- UWIND - Average windspeed over spillet in X direction (m/sec).
- VWIND - Average windspeed over spillet in Y direction (m/sec).
- WVEL - Total magnitude of windspeed over spillet (m/sec).
- DEPLOC - Average depth under spillet (meters).
- HTLOC - Average tidal elevation around spillet (meters).

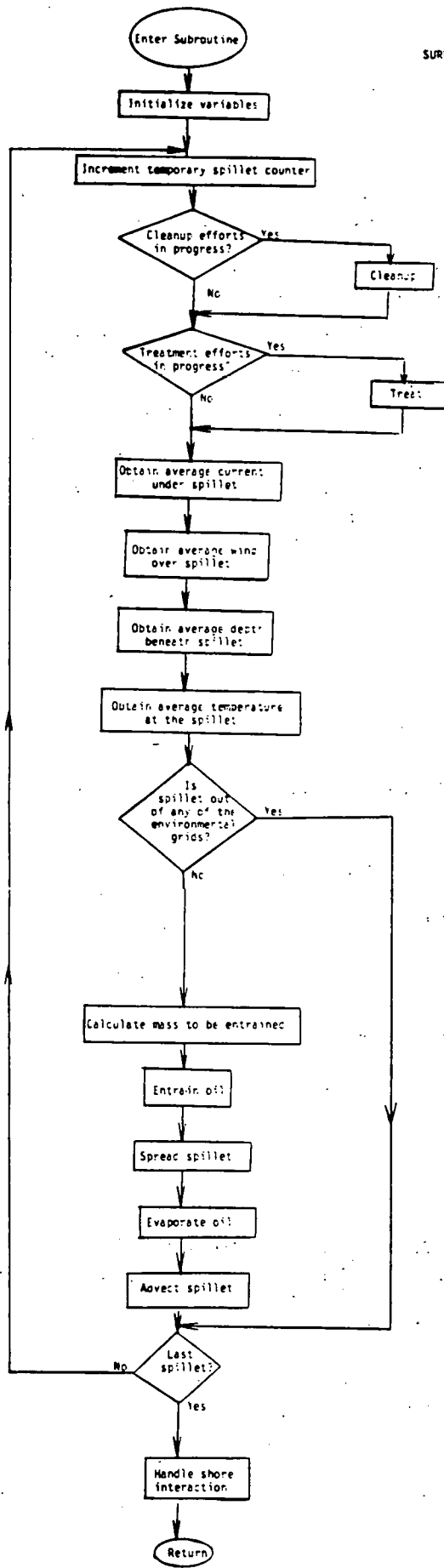


Figure IV.-34. Flowchart for subroutine SURFES.

Subroutine TREAT

This subroutine, see Figure IV-35 for its flow chart, handles the chemical treatment of the surface slicks. A number of treatment efforts may be in progress at any one time. Within range of a treatment effort, spilllets are treated in the order in which they occur, i.e., if the fifth, seventh and twelfth spilllet fall within range of a treatment effort, the fifth, then the seventh and finally the twelfth would be treated by this effort. If the area treated is less than the area of a spilllet, then only a fraction of the spilllet is treated and the next treatment effort is dealt with. In this case, the fraction of oil which is dispersed is the ratio of the treated area to the total spilllet area. If, on the other hand, the area to be treated is greater than that remaining in the spilllet, then it is treated and the next spilllet is treated, etc. The percentage of oil dispersed in this case is defined by PCHEM. The area treated is stored and in the next time step, only the remaining untreated area is treated.

CALLED FROM: SURFES

SUBROUTINES CALLED: DIST, REMOV

Important Local Variables:

- TRAREA - Area to be treated at this step (meter²).
- DIS - Distance between the center of treatment effort and the center of spilllet of interest (meters).
- SPAREA - Area of the spilllet which has not been treated (meters²).
- PER - Fraction of oil which is entrained.
- XMSDP - Mass entrained by this effort (metric tons).
- SUMAS - Mass entrained this step (metric tons).
- AMNT - Area treated (meters²).

Subroutine VELC

This routine, Figure IV-36, calculates from the appropriate fixed grids, the water depth, the tide height and the current velocities at each of the corresponding floating grid locations using a bilinear interpolation (see the description of subroutine PARTV for a discussion of the bilinear interpolation). If the floating grid comes too close to the edge of the corresponding fixed grid for proper interpolation, a warning is written. The program will continue to execute but interpolation errors are probable at this point or in other routines of the model. Due to the space staggered system and the possible rotation of some of the grids, each grid is interpolated separately.

CALLED FROM: CNVRTZ, VELCT

SUBROUTINES CALLED: ROTAT

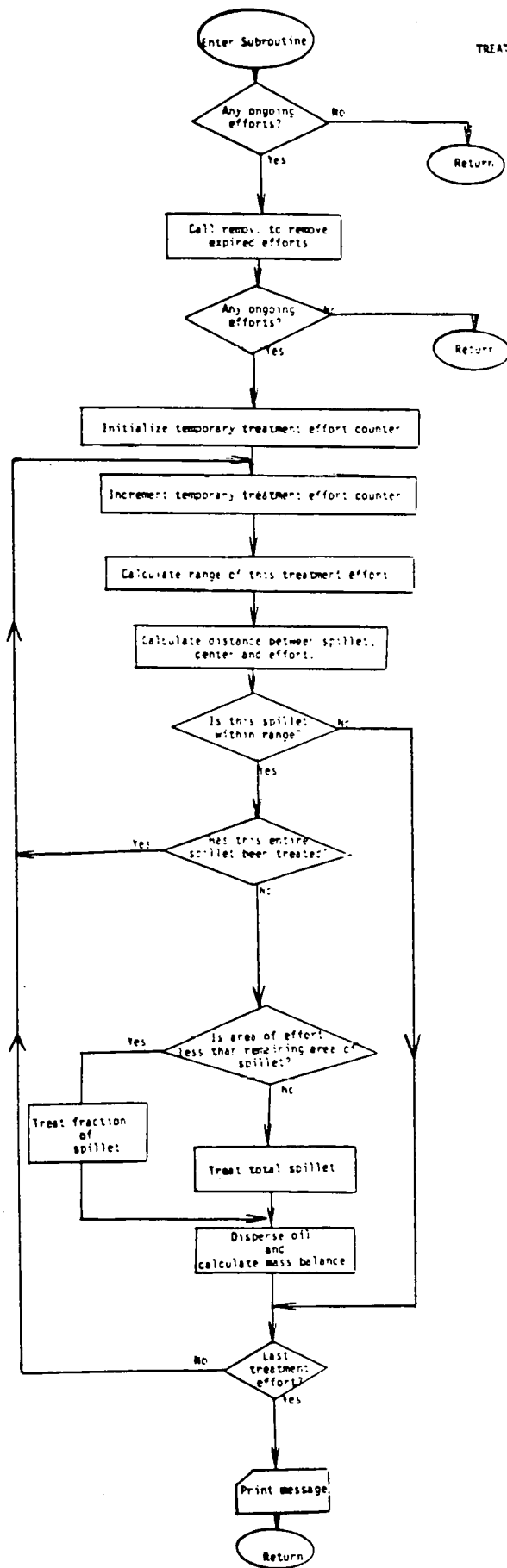


Figure IV.-35. Flowchart for subroutine TREAT.

VELC

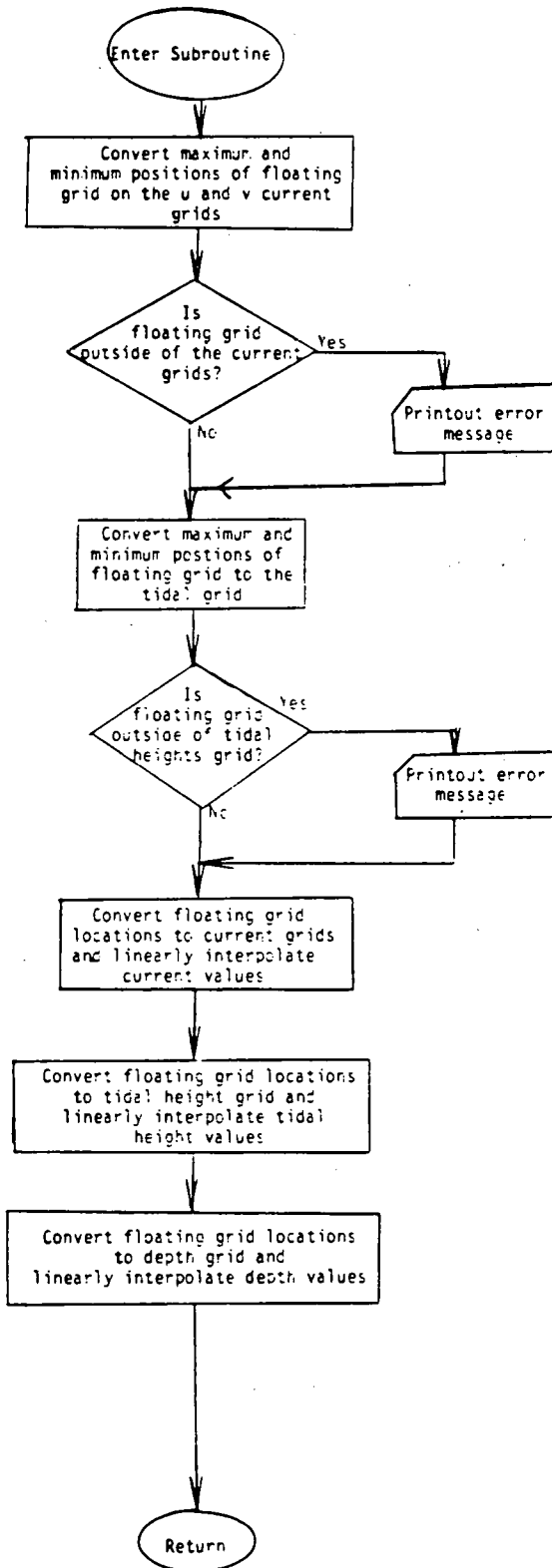


Figure IV. - 36. Flowchart for subroutine VELC.

- DIS - Distance between the center of treatment effort and the center of spillet of interest (meters).
- SPAREA - Area of the spillet which has not been treated (meters²).
- PER - Fraction of oil which is entrained.
- XMSDP - Mass entrained by this effort (metric tons).
- SUMAS - Mass entrained this step (metric tons).
- AMNT - Area treated (meters²).

Subroutine VELC

This routine, Figure IV-36, calculates from the appropriate fixed grids, the water depth, the tide height and the current velocities at each of the corresponding floating grid locations using a bilinear interpolation (see the description of subroutine PARTV for a discussion of the bilinear interpolation). If the floating grid comes too close to the edge of the corresponding fixed grid for proper interpolation, a warning is written. The program will continue to execute but interpolation errors are probable at this point or in other routines of the model. Due to the space staggered system and the possible rotation of some of the grids, each grid is interpolated separately.

CALLED FROM: CNURTZ, VELCT

SUBROUTINES CALLED: ROTAT

Important Local Variables: None

Subroutine VELCT

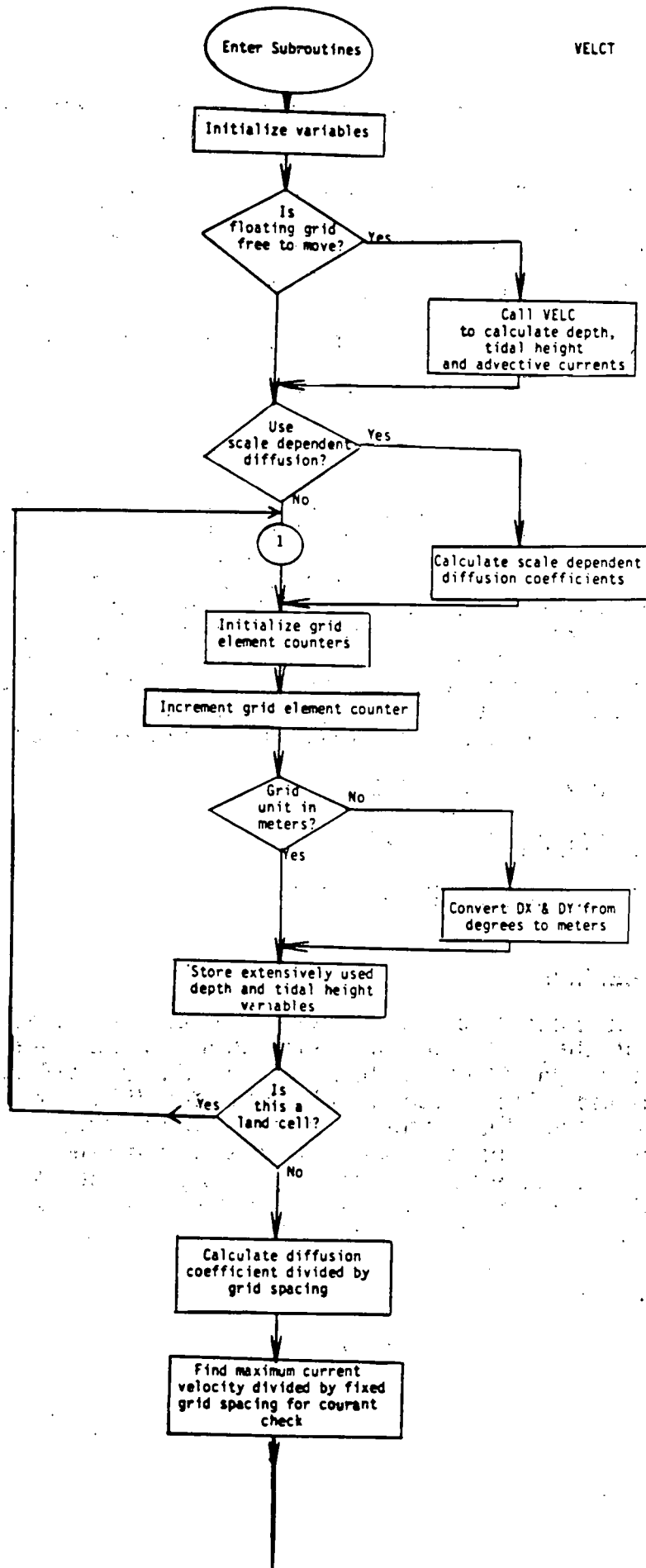
This subroutine, Figure IV-37, calculates the diffusion velocities at each of the grid nodes and adds these to the advective terms. If the number of particles is less than NCRIT, the diffusion velocity is not calculated. The procedure calculates the diffusion coefficients and then locates the four closest concentration nodes. The difference is determined in the X,Y, and Z direction and used to calculate the three velocity components. If the large scale mode is used, the horizontal velocity components must be converted to degrees/sec. The maximum advective and diffusive velocities (divided by the grid spacings) are also determined.

CALLED FROM: SUBSUR

SUBROUTINES CALLED: DIFF, VELC

Important Local Variable: None

VELCT



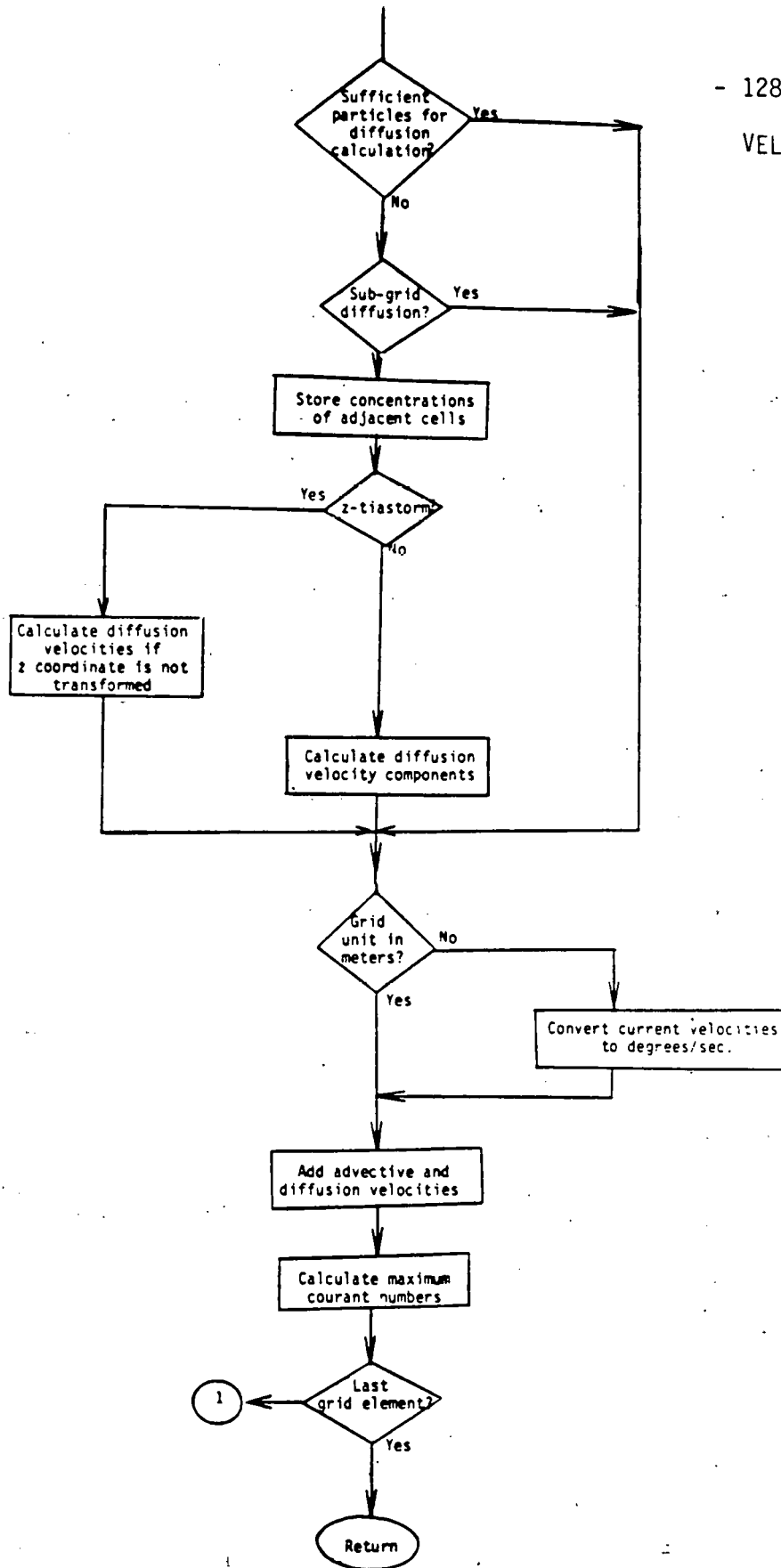


Figure. IV. - 37. Flowchart for subroutine VELCT.

APPENDIX V. Input Programs

This Appendix gives the details necessary to use the input programs GRIDS and CHECDATA.

A. GRIDS

As described in Chapter II, this program serves to format environmental data for input into either a preview run or a complete simulation. The general flow through this program is shown in Figure V-1. The first step is to read the grid control variables i.e., the variables that control the execution of the run. These variables are shown in the upper half (above the dotted line) of Table V - 1 in the order in which GRIDS will read them. The subroutines READI and READF described in Appendix IV are used to input these parameters. The formats required by READI and READF are specified in Appendix I, Section D2.

The next step is to read the grid definition variables, i.e., the variables that define the grid, such as, number of grid elements, the angle of rotation, the various names, etc. This is done in subroutine READU which again uses READI and READF to read fixed and floating point variables, respectively. Two new subroutines are also called in READU; READN2 and READN3. The structure of these subroutines is identical to READF, the only difference being that they are used to input character data, i.e., grid names and units, instead of numerical values. READN2 will enter an 8 character name and READN3 is used to enter a 12 character name. The format for READN2 is:

(7X, 2A4, 5X, A8)

while that for READN3 is:

(3X, 3A4, 5X, A8)

These formats are to be compared to that of READF:

(F15.5, 5X, A8)

The variables input in this step, their order of input and the appropriate input subroutine is shown in the lower half of Table V - 1.

Following the entry of GRID control parameters and environmental definition variables the title of the environment grid is checked to see that it is one of:

'BATHYMETRY'
'TEMPERATURE'
'WIND VEL'
'UTID CURRENT'
'VTID CURRENT'
'TIDE LEVEL'

If the grid title is not one of these spelled exactly as above, an error message is written and the program stops.

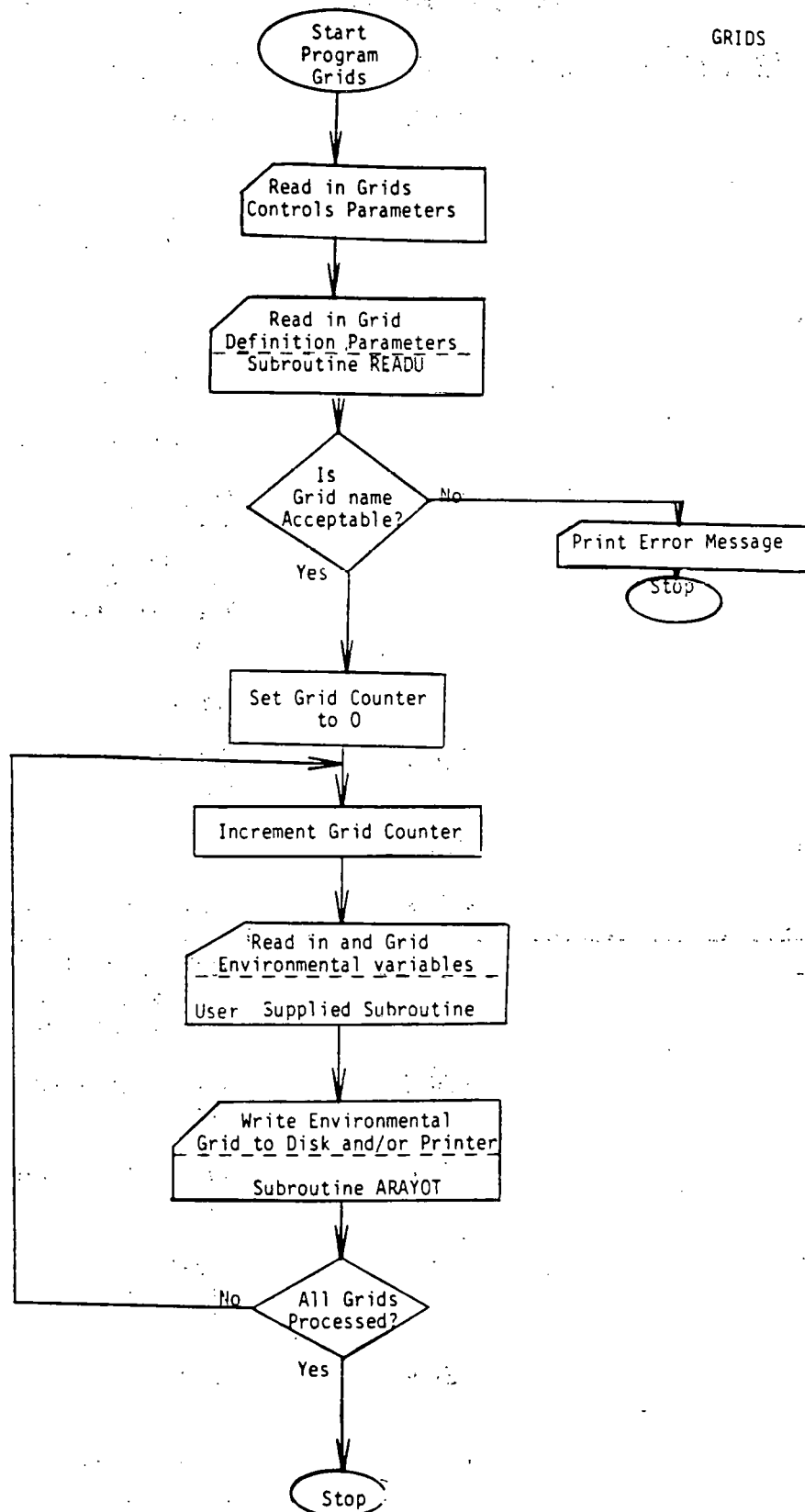


Figure V.-1. Flowchart for input program GRIDS.

Table V - 1. List of Variables for GRIDS
Input Parameters - in order of entrance

<u>Input Parameters</u>	<u>Subroutine used</u>	<u>Description</u>
NPRTA	READI	Print control parameter. -1 - no diagnostic print out 0 - limited print out - prints out line to tell the step and the time.
print		1 - full print out - formatted out of what goes to cards, disk or tape.
NO	READI	Number of variables per grid.
NU	READI	Format control for cards or disk printout of environmental grids. 1 - unformatted real variables 2 - unformatted integer variables 3 - formatted real variables 4 - formatted integer variables
NUM	READI	Number of steps to be written out.
ND	READI	Unit number data is to be written to.
NUNIT	READI	Unit number data is to be read from.
DT	READF	Time step between data values.

ISCAL	READI	Control parameter for scale mode. 1 - small scale (meters) 2 - large scale (degrees)
IMAX	READI	Number of elements in the x direc- tion.
JMAX	READI	Number of elements in the y direc- tion.
ANGLE	READF	Angle measured in the counter clock- wise direction from East to the positive x-axis (in degrees).
XS,YS	READF	Spacing between grid lines in x and y direction (in meters or degrees).
XL,YL	READF	Location of (1,1) point of the grid (in Longitude and Latitude).
TITLE	READN3	- 12 character variable giving the name of the grid. This must be

correct in order to print out.

VAR1, VAR2	READN2	8 character variable giving the name of the variable in the grid.
UNITS1, UNITS2	READN3	12 character variable giving the dimensions for print out. If there is only one grid, VARS2 and UNITS2 are not needed.
UNITS3	READN2	8 character variable giving the units of XS and YS.

Other Variables in GRIDS

NAMCH	Correct titles to be used by the program, if these are not correct and in the order required by the main program, the run will terminate.
-------	---

ARRAY1, ARRAY2	The values of the grid data when the data is real. If there is only one grid, ARRAY1 is used.
----------------	---

MARAY1, MARAY2	The values of the grid data when the data is integer. If there is only one grid, then MARAY1 is used.
----------------	---

If the grid title is acceptable then a do loop is executed over the number of time steps, NUM, for which the particular grid is to be updated. In this loop, the user supplied subroutine, FIX, is employed to read the environmental data values and then to perform the necessary operations to work them into a rectangular grid.

Finally, this grid is output by the subroutine ARAYOT. This subroutine is an exact duplicate of ARAYIN discussed in Appendix IV except all READ statements have been changed to WRITE statements. The appropriate output formats are described in Appendix I, section A.

A brief summary of the GRIDS and its subroutines is included below.

- 1) Main Section - This section reads in several input parameters, does a check on the title, then loops over the number of grids to be entered, by the variable NUM.

Calls Subroutines READI, READU, Fix, and ARAYOT.

- 2) Subroutine READU Reads in all necessary input variables and units. Calls Subroutines READI, READF, READN3, and READN2.

- 3) Subroutine FIX -The Subroutine must be written by the user. It reads the environmental data and does any necessary calculations or manipulations needed to work the data into a form compatible with the structure of ARRAY1 and/or ARRAY2. In the example, a current data set is read in and converted to degrees/sec.

- 4) Subroutine ARAYOT - Writes the variables to unit ND in the format defined by the previous parameters.

- 5) Subroutine READI, READF, READN3, READN2 - reads and checks input parameters. If the spelling is incorrect or the title is not in the correct column, the run terminates.

Formats READI (I15, 5X, A8)
READF (F15.5, 5X, A8)
READN3 (3X, 3A4, 5X, A8)
READN2 (7X, 2A4, 5X, A8)

B. READATA

The purpose of this Subroutine is to verify that the environmental data is in the proper format for input to the preview program or the full simulation. The Subroutine is extremely straight forward. Five control parameters are read specifying the print control, the number of variables per grid (1 or 2), the format of the data, the number of grids (time steps for which the environmental grid is to be updated) to be read and the unit number from which the data is to be read. Table V - 2 lists all input variables to READATA. All of these variables being fixed point or integer are read in with the Subroutine READI (see Appendix IV for a description of READI and Appendix I, Section 2 for a description of the appropriate format). A do loop is then executed over the number of

grids. The interior of this do loop is an exact duplicate of the working part of the Subroutine ARAYIN described in Appendix IV including the checks that are made on the title of the environmental array.

Table V - 2. List of Variables for READATA displayed in order of entrance.

Input Variable	Subroutine Used	Description
NPRTA	READI	Print control parameter (see program GRIDS).
NO	READI	Number of variables per grid.
NU	READI	Format control (see GRIDS).
NUM	READI	Number of steps to be read in.
ND	READI	Unit number form which data is to be read.
ISCAL	READI	Control parameter for scale mode. 1 - small scale (meters) 2 - large scale (degrees)

Appendix VI: Output Programs Descriptions

This appendix is included to provide the user with the details necessary to run the output programs. There are six such programs which are either run independently or in conjunction with one or more of the others. The relationship between the various programs are discussed in Chapter V and will only be repeated here as necessary for their use. All plots are generated with standard CALCOMP software.

A... PLOTMASS

A detailed flow chart for PLOTMASS is presented in Figure VI-1, a simpler flow chart is shown in Figure 8. This program requires two different sets of control parameters in addition to the input data available from the simulation model. One set controls the run itself, specifically how many timesteps are to be used, NST, and the number of simulated data sets to be plotted, NPLOT. These two parameters are read in with the subroutine READI discussed in Appendix IV. The second set of input parameters read as one logical record controls which variables in the mass balance are to be plotted. The format used to read these parameters is given by:

```
READ (5,200) NUN, NATM, NBIO, NBOT, NCLN, NLOS, NSHR, NSUR, NSUS, NDMP
200 FORMAT (2X,10I4)
```

The meaning of each of these variables is outlined in Table VI-1.

The results of two different runs may readily be compared by specifying NPLOT equal to 2 and NUN equal to 0. The first set of data will then be plotted with solid lines and the second with dashed lines on the same plot.

A second option in this program is to plot the same data set a number of times in different ways on different plots. In this case NPLOT would be set equal to 1 and NUN to 1.

The IBM Job Control Language for the output data set required to run this model is:

```
// FT FOOT DD DS NAME = MASS. PLOT,
//          DISP = (NEW,CATLG).
//          UNIT = SYSDA,
//          DCB = (RECFM = UBS, BLKSIZE = 1954),
//          SPACE = (TRK(2,2))
```

An example plot is shown in Appendix VIII.

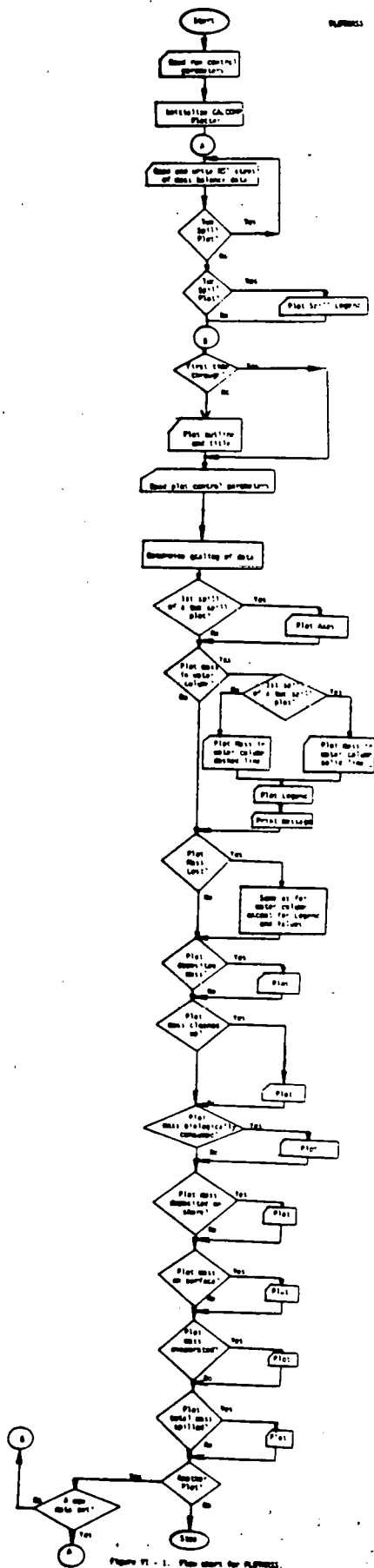


Figure VI - 1. Plot sheet for PLUMESS.

Table VI-1

Variable	Input to Plotmass		
	Range	Format	Description
NST	1-100	READI	# of model timesteps in plot
NPLOT	1-6	READI	# of data sets on one plot
NUN	0-1	14	0-Use same mass balance data 1-Read in new data
NATM	0-1	14	0-Do not plot mass in atmosphere 1-Plot mass in atmosphere
NBIO	0-1	14	0-Do not plot mass consumed biologically 1-Plot mass consumed biologically
NBOT	0-1	14	0-Do not plot mass deposited on the bottom 1-Plot mass deposited on the bottom
NCLN	0-1	14	0-Do not plot mass cleaned up 1-Plot mass cleaned up
NLOS	0-1	14	0-Do not plot mass lost to an open open boundary 1-Plot mass lost to an open boundary
NSHR	0-1	14	0-do not plot mass deposited on shore 1-Plot mass remaining on the surface
NSUS	0-1	14	0-Do not plot mass in the water column 1-Plot mass in the water column
NDMP	0-1	14	0-Do not plot total mass spilled 1-Plot total mass spilled

Program PARTICLE

This program (Figure VI - 2) is used to change the resolution of a floating grid using data which has been previously written to disk. The particle parameter data set is read in the main program and used by subroutine PRINT. The user specifies the number of grid elements in the X and Y directions. These values are then used to calculate a new floating grid and new concentration values. The new concentration values are then written out to disk for use in the OUTPUT programs. The subroutines used to determine the new grid location and shape, GRIDEX, to calculate the hydrocarbon concentration on this grid, CONC, and to write and print the results of these calculations, PRINT are identical to those used in the main simulation. All three subroutines are described in detail in Appendix IV.

PARTICLE

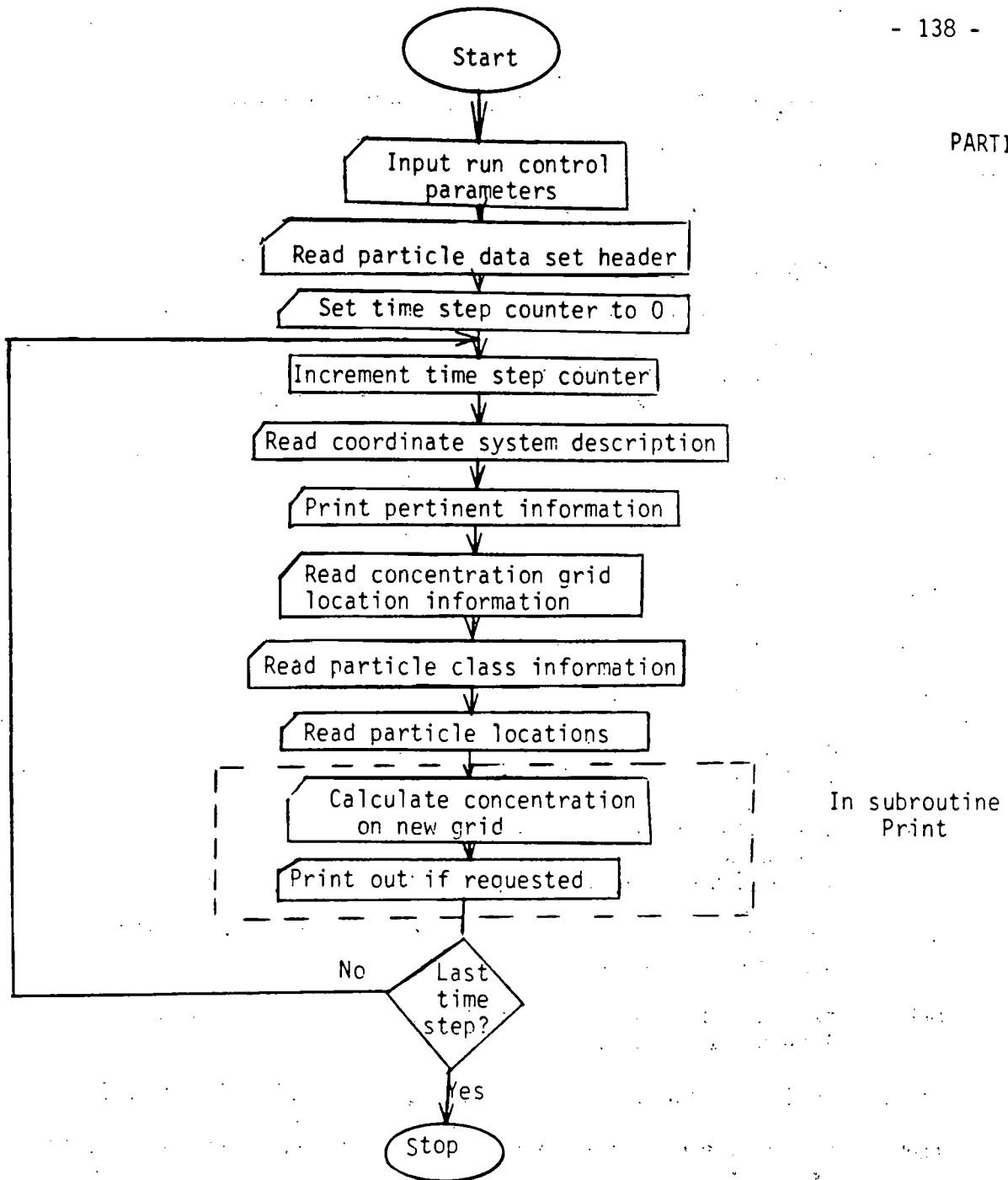


Fig. VI -2 Flow chart for Program PARTICLE

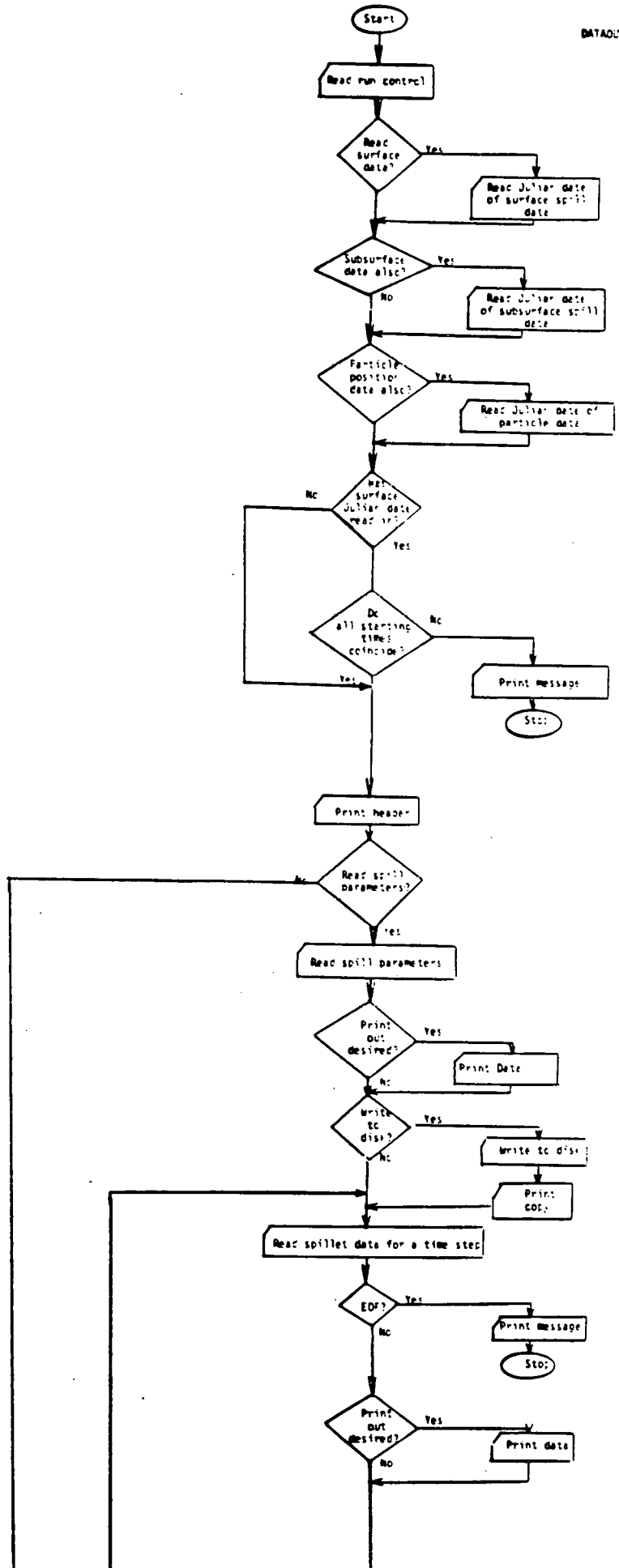
Calls Subroutines CONC, GRIDEX, PRINT, READI AND READN2.

Input Variables (In order)

- NMAX - maximum number of particles allowed.
- NSTEP - number of time steps this program is to be run.
- ISCAL - size scale parameter. This must be the same as the previous simulation run.
 - 1 - does horizontal calculations in meters.
 - 2 - does horizontal calculations in degrees.
- NPTFLT - print control for floating grid information. This is the print interval in number of steps.
- IMSUB - new number of grids in the x direction.
- JMSUB - new number of grids in the y direction.
- KMSUB - new number of grids in the z (vertical) direction.
- KPRTC - concentration print control parameter.
- KPRTP - particle position print control parameter, print out at this interval of time steps.
- NPRD - disk data set print control parameter.
 - 0 - no data sets written out this step.
 - 1 - at least one data set written out this step.
- NPRC - concentration disk data set print parameter, write out at this interval of steps.
- NPRP - particle disk data set print parameter, write out at this interval of steps.
- UNITS3 - units of new grid point spacing, e.g., DEGREES, METERS, etc.
- NUNCN - the device number to which the new concentration grid is to be written.
- NUNPT - the device number from which the particle positions are to be read.

C. DATAOUT

This program, flowcharted in Figure VI-3, is used to prepare data output by the simulation program for input to the surface and subsurface plotting programs. It may also be used to printout the output of the simulation program. The user may select whether this printout is to be simply a copy of the simulation data sets and/or a printout similar to that available from the simulation mode, i.e., formatted for easier interpretation. These options are selected by specifying different combinations of the six run control variables. The run control parameters,



DATAOUT CONT'D.

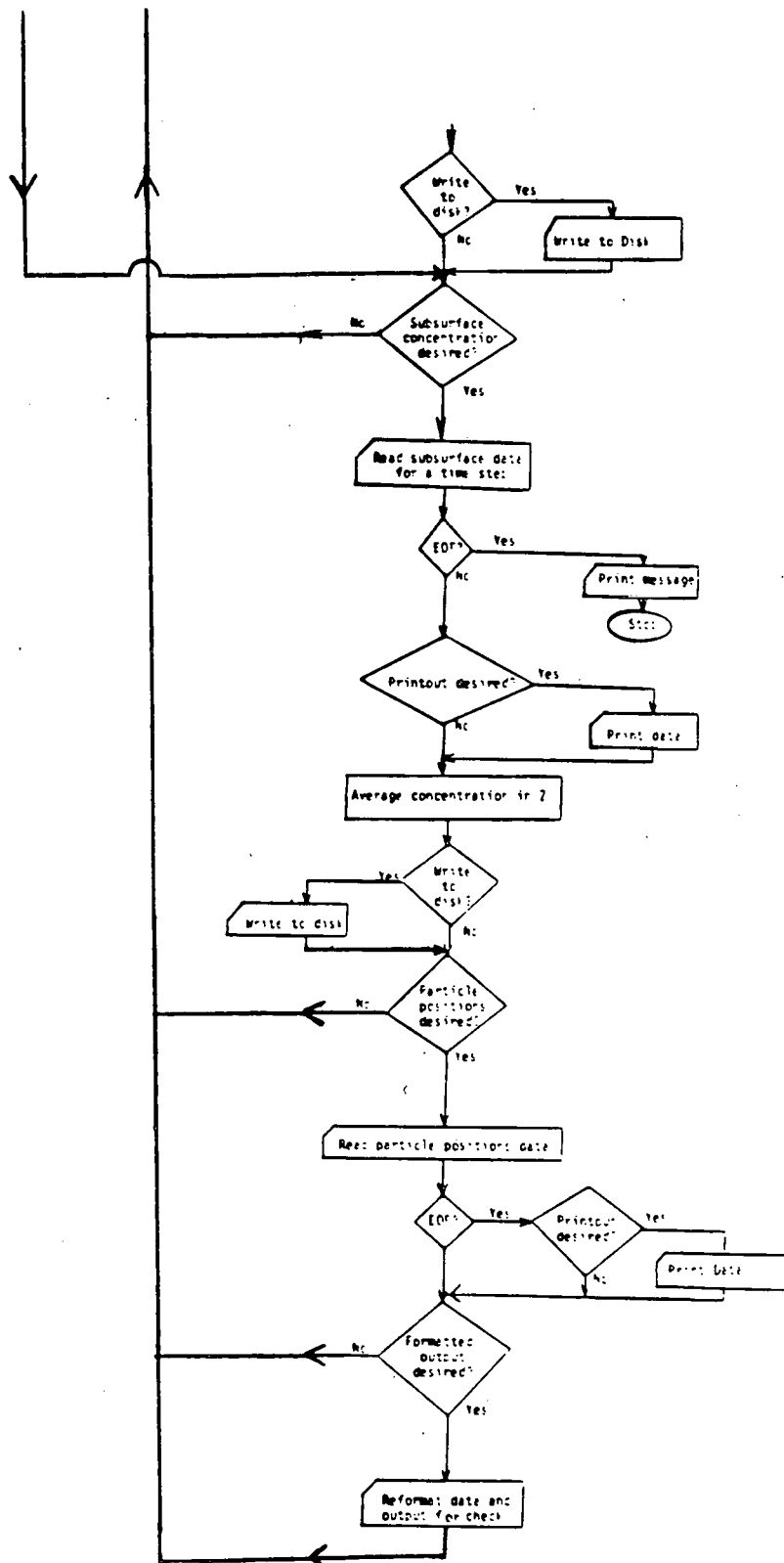


Figure VI - 3. Flow chart for Program DATAOUT.

tabulated in Table VI-2, are read in by the subroutine READI, discussed in Appendix IV. The variable NPRT is used to control the output of this program while the variables NRDSP, NRDCN and NRDPT determine whether or not spilllet information, a concentration distribution and/or particle information is to be read. If these variables are zero then the associated data sets are not read. If they are not zero, then their value specifies the unit number from which the data is to be read.

The program will determine all grid elements in the horizontal for which the vertically averaged concentration exceeds the value of the run control parameter: CCUT. The location of these elements is output to the disk data set designated as input to the plotting programs.

The remaining run control parameter, ISCAL, is required by that part of the program calculating the location of the grid elements with a hydrocarbon concentration exceeding CCUT. If ISCAL = 2, the locations are written to disk in longitude and latitude. If ISCAL = 1, the locations are written to disk in meters from the fixed depth grid origin.

The user must supply the run control parameters described above, data set(s) from which the oilspill output data will be written and the data set to which the reconfigured data will be written. This last data set is unformatted, variable locked. The IBM Data Definition statement defining it is:

```
//FTO F001 DD DSN=name, DISP=(NEW,CATLG)
//   DCB=(RECFM=VBS, LRECL=44, BLKSIZE=4404),
//   VOL=SYSDA,SPACE=(4404,(10,10))
```

Input Variables for Program DATAOUT:

- NPRT - print control parameter.
 - 1 write reduced output to disk.
 - 0 no printout.
 - 1 print data as read in.
 - 2 print data as formatted output.
 - 3 print both formatted and as read.

- ISCAL - scale mode parameter, must be the same as specified in the original simulation.

- NRDSP - print control parameter for spilllet data set.
 - 0 - spilllet information not read in.
 - >0 - spilllet information read in from this unit number .

- NRDCN - print control parameter for concentration data.
 - 0 - concentration data not read in.
 - >0 - concentration data read in from this unit number.

- NRDPT - print control for particle data set.
 - 0 - particles not read in.
 - >0 - read particle parameters from this unit number.

- CCUT - controls the lowest value of concentration to be written out. This is read in as parts per thousand and converted to parts per billion for the printout.
- CONC(IMSUB,JMSUB,KMSUB) - 30,30,10 - concentration of the levels of the water column (ppt).
- CC(IMSUB,JMSUB) - 30,30 - averaged concentration over the water column (ppt).
- NSUM - number of elements exceeding CCUT.
- CT(NSUM) - 899 - concentration of those elements which exceeds CCUT (ppb).
- XG(NSUM), YG (SNUM) - longitude and latitude of these concentration values. If AD = 0, these are returned in meters.
- THIC - thickness of the spilllet (meters).
- ZT(MMAX) - transformed depth of particle.
- DX,DY - grid spacing in X and Y direction (meters).
- X,Y,Z - particle positions.

See common blocks SPIL, PTYP, and DPTH for other variables.

D. Program CHECDATA

This program (figure VI-4) checks the data set output by the program DATAOUT. This data set, which includes the spilllet parameters and concentration parameters, is read and printed in an easy to read fashion. The only input parameters required are those which specify the device from which the data is to be read, NUNIT, and the parameter, NRDCN, which specifies whether or not the subsurface concentration grid is included in the input data set. If NRDCN is equal to zero, then the subsurface concentration grid is not included. The program terminates after it has been read and printed all of the data available.

The variables used are the same as in DATAOUT. (Also see common block SPIL).

E. PROGRAM PLOTMAP

This program plots a map of the spilled oil exceeding a given thickness on the surface and exceeding a given concentration beneath the surface. The data is read in for the designated number of steps and the maximum extent of the oil is determined in terms of longitude and latitude. This defines the origin and the conversion factor, SCAL, required to convert degrees of longitude and latitude into plotter coordinates, inches. The routine then loops over the total number of time steps, generating a plot at time step intervals of HR. The spilllets are plotted

CHECDATA

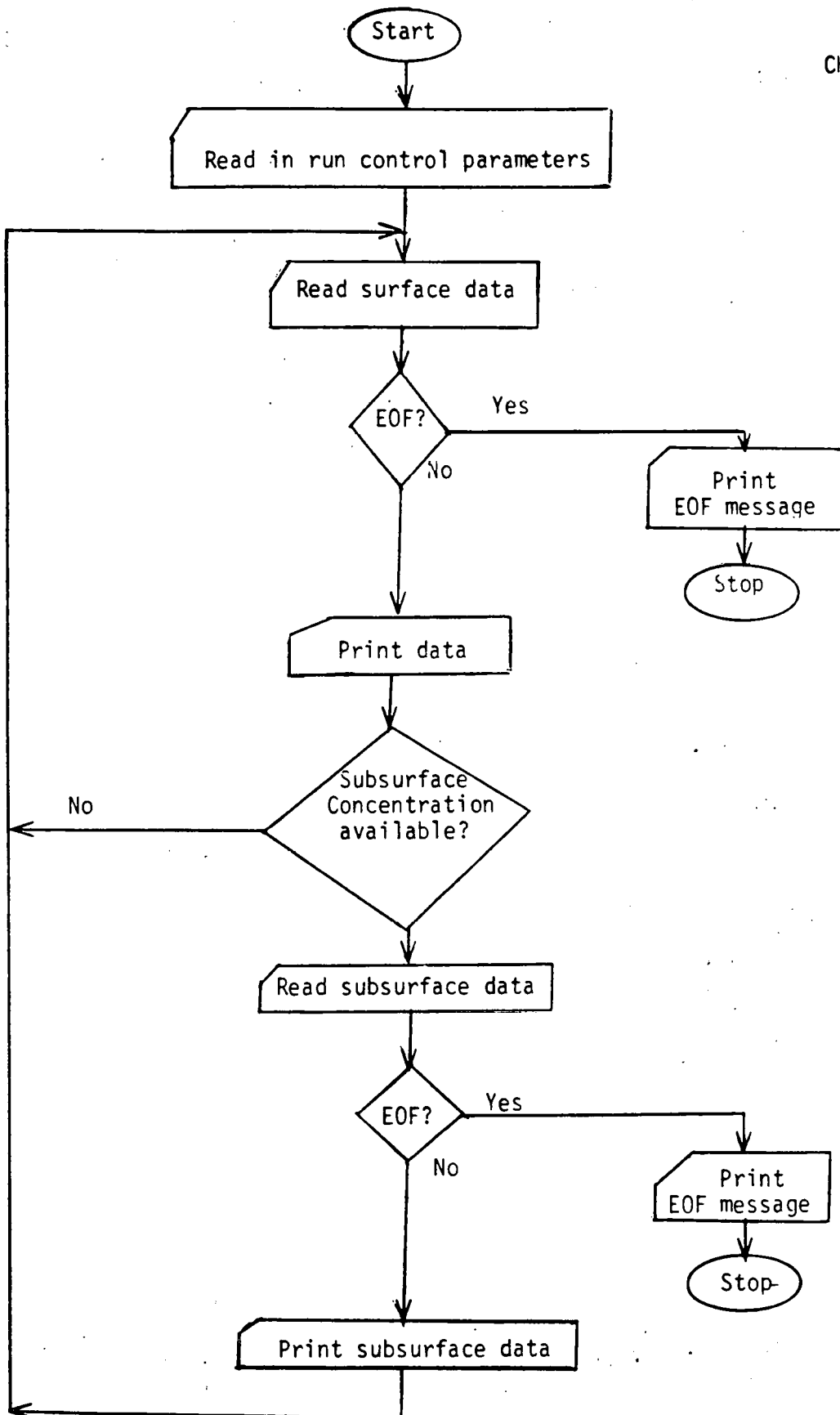


Figure VI - 4. Flow chart for Program CHECDATA.

as circles while the subsurface area exceeding a specified concentration values is outlined. The outline is constructed starting at the north and moving clockwise. The outline is started at the top (north) left hand corner of the concentration values if the floating grid is rotated. The number of data sets to be used is determined by NPLOT and the cases are plotted in order of ascending device number. The routine can only plot a maximum of two cases at one time. The first case is plotted using solid lines and the second case using dashed lines. The legend which includes a scale and other information is plotted in the upper right hand corner. Tick marks for longitude and latitude are drawn around the edges in intervals of a tenth of a degree. An example of such a plot is given in Appendix VIII. The two input parameters XLNG and YLTD give the interval at which the values of longitude and latitude respectively, are to be written. See Figure VI-5 for a flow chart of Plotmap.

A shoreline may be plotted by indicating the number of points to be plotted which is controlled by the parameter NSHOR. Plotmap calls subroutine READI, READF and POSIT in addition to standard CALCOMP routines.

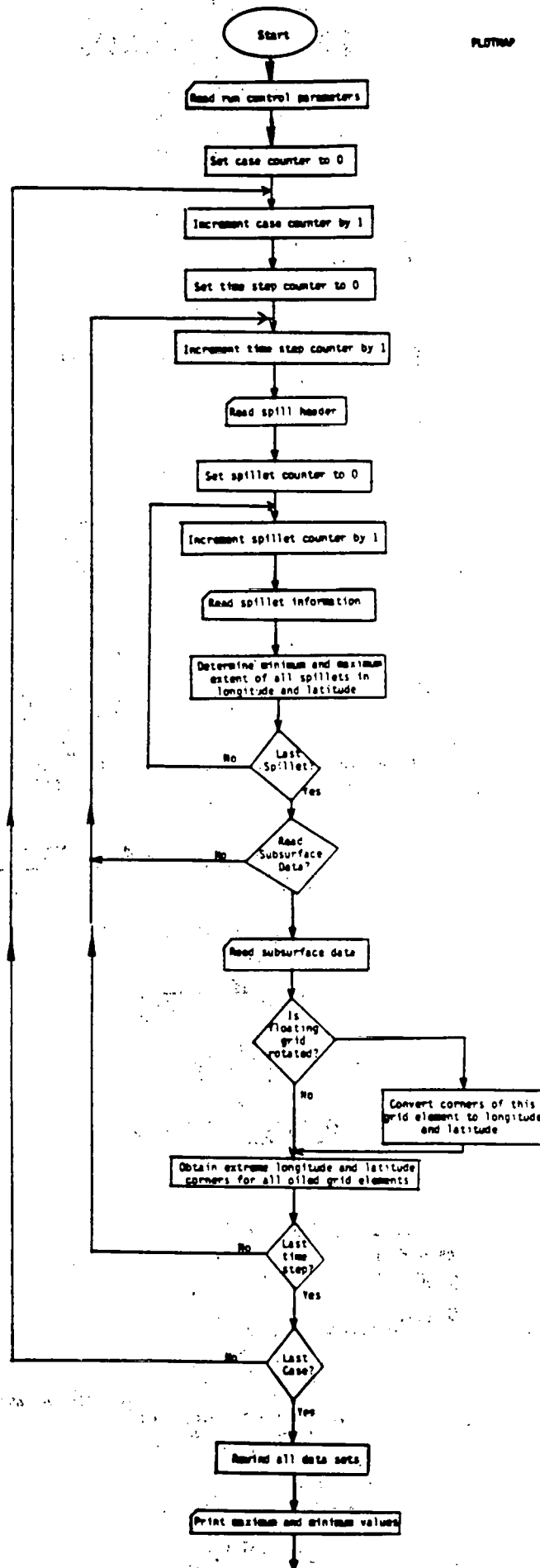
Input Variables for Plotmap:

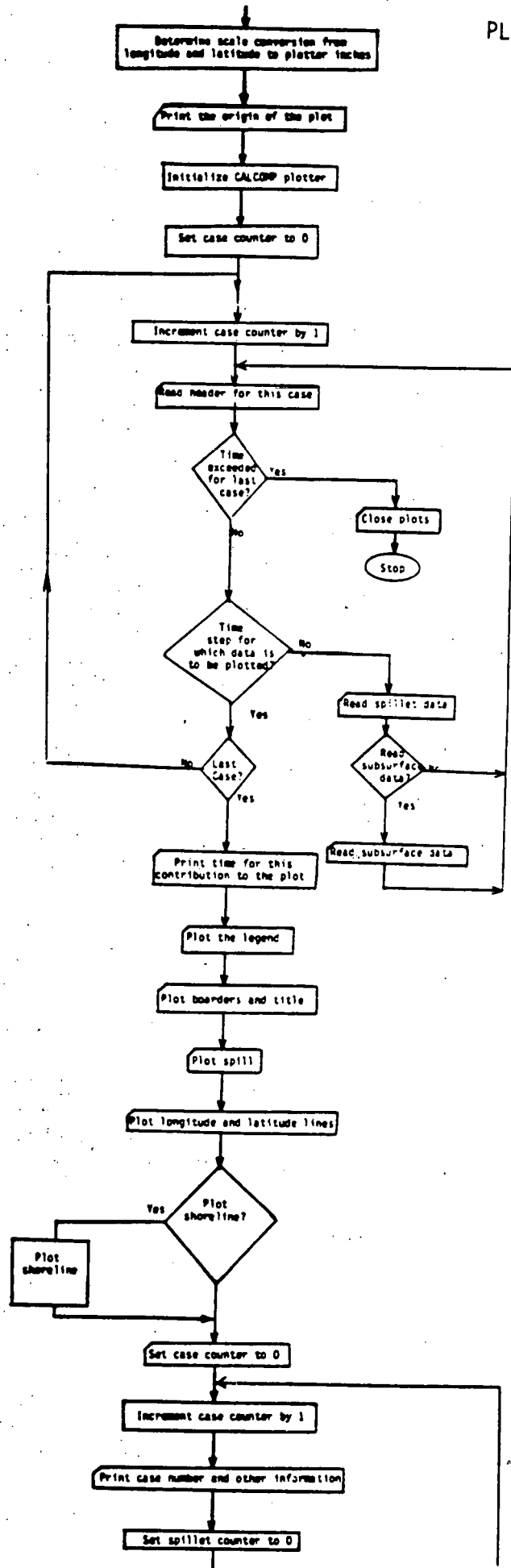
- NPLOT - number of cases which are to be plotted. This indicates the number of input units to be used.
- NSTEP - number of steps to be read.
- HR - interval for plotting. (Hours)
- THICK - minimum thickness of spillet to be plotted (meters).
- XLNG - interval between longitude tick marks (degrees).
- YLTD - interval between latitude tick marks (degrees).
- NRD10 - control parameter for subsurface outline
0 - plot surface spillet only
1 - plot surface and subsurface spillet.
- ISCAL - scale mode control parameter
2 - floating grid is not rotated.
1 - floating grid may be rotated.
- NSHOR - number of shoreline points to be plotted.

Other important variables for PLOTMAP:

- XMIN, XMAX - maximum extent of spillet and subsurface grids in longitude. (If the floating grid is rotated this is in meters).
- XMIN, YMAX - maximum extent of spillet and subsurface grids in latitude. (If the floating grid is rotated, this is in meters).
- NUMELM - number of elements which exceed the minimum cut.

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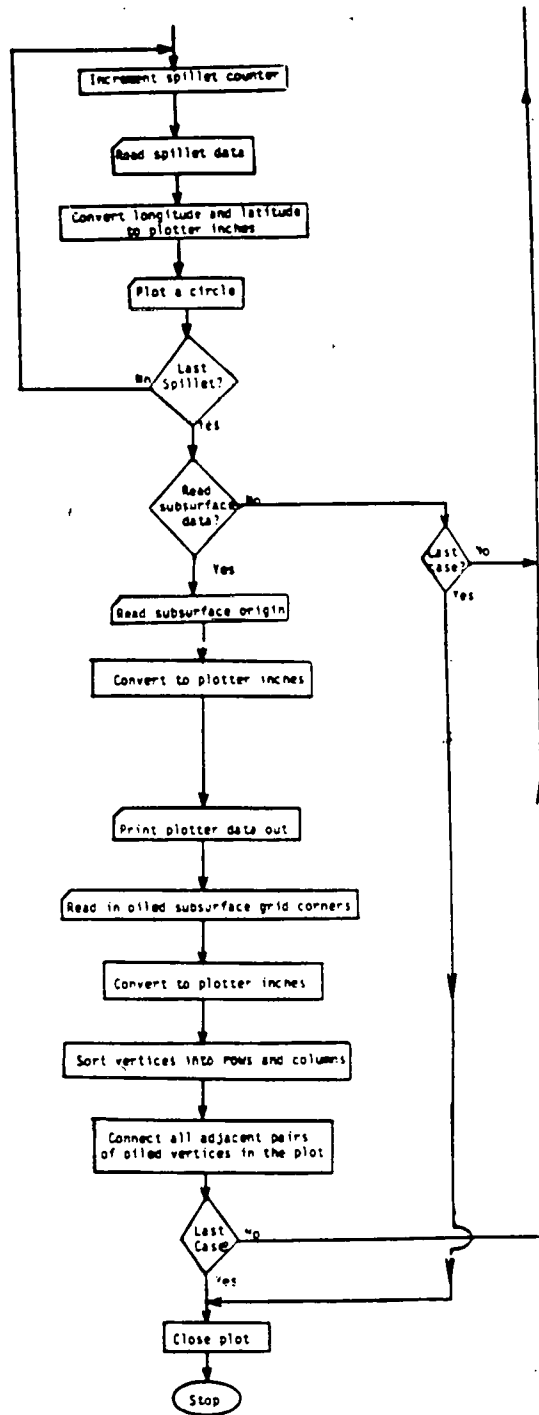


Figure VI. - 5. Flowchart for Program PLOTMAP.

- XSIT, YSIT - site of spill, location of first spilllet at time zero is used (longitude and latitude).
- XOR, YOR - origin used for plotting, this is located approximately at the middle bottom of the plotted area (longitude and latitude).
- SCAL - scale factor for plot (degrees/inch).
- XSPIL, YSPIL - center of spilllet (longitude and latitude).
- RSPIL - radius of spilllet (meters).
- THIC - thickness of spilllet (meters).
- XOILMN, XOILMX - minimum and maximum extent of subsurface oil (longitude).
- YOILMN, YOILMX - minimum and maximum extent of subsurface oil (latitude).
- DXT, DYT - grid spacing of floating grid elements in X and Y direction (meters).
- XG, YG - position of grid element (longitude and latitude).
- CG - concentration of grid element (ppb).

F. Program PLOTAREA

This program (Figure VI-6) will generate, using standard CALCOMP software, a figure of area covered by the surface and subsurface oil as a function of time. It calculates the area of each spilllet but only includes this area if the thickness of the spilllet is above the user defined minimum. The user determines which portion to plot by use of the variable, NAR. The subsurface grid areas are added up to determine the area for which the subsurface concentration exceeds some user defined minimum value. The user may display the results of several simulated spills at once, the data to be plotted coming from data sets identified by consecutive unit numbers beginning with 1. Because a scale is involved, the case which covers the most area should be plotted first so that all other curves will remain within the figure borders. The scale is determined from the total area covered at the last time step for the data set on unit one. An example plot is contained in Appendix VIII.

Input Variables for PLOTAREA:

- NAR - control parameter.
- 1 plot surface only.
- 0 plot only subsurface area.
- 1 plot surface spilllets and subsurface area.
- NPLOT - number of cases (or data sets) to be plotted.

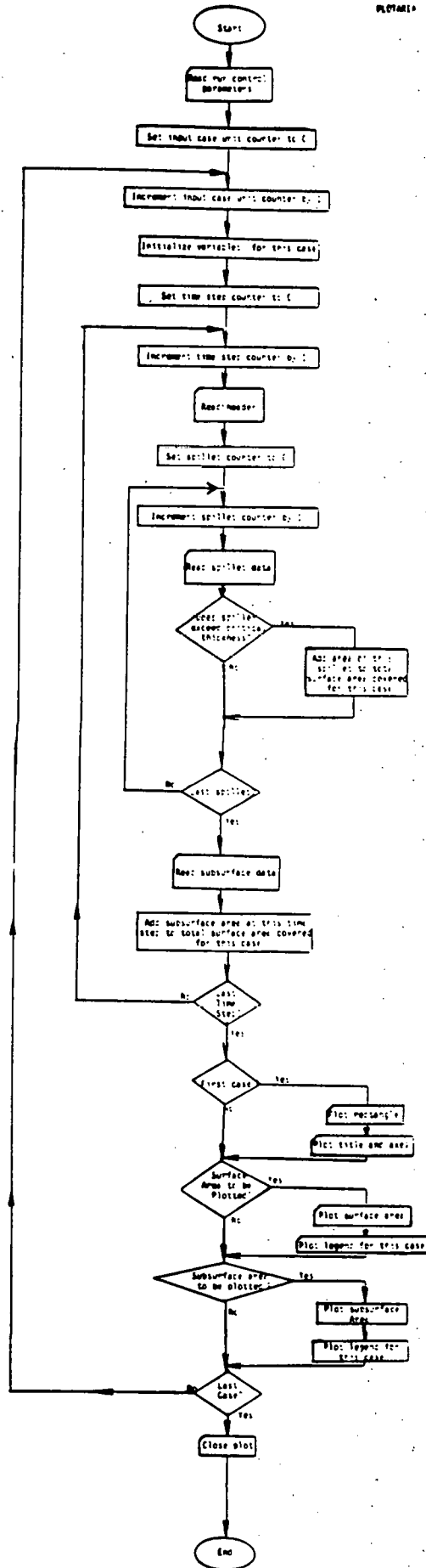


Figure 11. - 6. Flowchart for Program PLOTAREA.

THICK - minimum thickness of spillet to be plotted (meters).

NSTEP - number of steps to be plotted.

Other important variables of PLOTAREA:

TIME (NSTEP) - 103 - time of a model time step.

NSPIL - number of spilletts of a model time step.

XSPIL (NSPIL), YSPIL (NSPIL) - 30 - longitude and latitude of spillet center.

RSPIL (NSPIL) - 30 - radius of spillet (meters).

THIC - thickness of spillet (meters).

ASUR (NSTEP) - 50 - area of surface of a model time step (km²).

ASUB (NSTEP) - 50 - area covered by subsurface of a model time step (km²).

ATOT (NSTEP) - 50 - total area covered at the given model time step (km²).

XOILMX, XOILMN, YOILMX, YOILMN - maximum extents of subsurface concentration in longitude and latitude.

DX, DY - grid spacing in the X and Y direction (meters).

APPENDIX VII, PROGRAM LISTINGS

In this Appendix, listings of all programs are presented as used for the simulation discussed in Appendix IV. The two input programs are presented first followed by the simulation model and then the five output programs. Note that as presented here the PREVIEW program and the Main Simulation program are the same. If the user wishes to reduce the core requirements, a separate PREVIEW program may be created in which all subsurface routines are removed and the main subsurface routine, SUBSUR, is replaced by a dummy one. The arrays corresponding to the subsurface particle locations and properties should also be reduced to a value of 1.

The JCL listed with these programs is not always accurate. The JCL is compatible with the URI system but it may not be the most efficient. This is especially true for the space parameters and the allocation data set names as these names have been used for previous work. The DD statements at the end of the programs are not always used. The IBM 370 system at the University of Rhode Island uses the symbols /** as a JCL comment statement, thus these statements are ignored.

The program listings are listed in order in columns, as shown in Figure VII-1 through VII-9

COLUMN 1

COLUMN 2

```

//R235678 JOE (E11100), 'WRITE GFIDS ON DISK'
//* EXEC SCRDS*, DS*='URL.E3A1, RARPCB, BITWINT, UDIP*'
//* EXEC DSALLO
//DSR04 DD DS=URL.E3A1, RARPCB, BITWINT, UDIP, DISP=(,CATLG),
//* UNIT=SYSDA, SPACE=(7PA, (20, 10)),
//* DCC=(PDCP=VRS, BLKSIZ=1954)
// EXEC POPGCC, REGION, GO=120R, P1='SYSOUT=(C,,2019)',
// P3='SYSOUT=(C,,2019)'
//PORT.SYSIN DD *
C
C THIS PROGRAM PUTS ANY DATA AVAILABLE IN THE PROPER FORMAT
C FOR USE BY THE GRID SIMULATION. THIS PROGRAM DOES NOT HAVE
C TO BE USED BY THE USER WHEN RUNNING A SIMULATION BUT
C CAN BE USED TO FACILITATE DATA HANDLING.
C THE VARIABLES ARE DESCRIBED IN THE SUBROUTINE
C ARAYIN WITH THE EXCEPTION OF :
C   WDIR: - THIS IS THE DIRTY FROM WHICH THE DATA IS READ.
C   NO: - THIS IS THE UNIT TO WHICH THE DATA IS WRITTEN.
C   WOP: - THIS IS THE NUMBER OF STEPS TO BE WRITTEN.
C
C .....
CORROD /DATA/ BAR(3), VAP1(2), NO, WUNIT, ISCAL,
1  VAR2(2), UNITS1(3), UNITS2(3), UNITS3(2),
1  IJAX, JMAX, ANGLE, XL, YL, XS, YS
1  EQUIVALENCE (RPAAT1(1,1), RPAAT1(1,1))
EQUIVALENCE (RPAAT2(1,1), RPAAT2(1,1))
DIMENSION RPARC(4,3)
DIMENSION ARAY1(30,30), ARAY2(30,30), RPAAT1(30,30), RPAAT2(30,30)
DATA PI, NO, WPT / 3.14159, 6, 1/
DATA RPARC(1,1), RPARC(1,2), RPARC(1,3) / 'DIRTY', 'DIRTY', 'DIRTY' //
DATA RPARC(2,1), RPARC(2,2), RPARC(2,3) / 'EPAAT', 'DIRTY', 'DIRTY' //
DATA RPARC(3,1), RPARC(3,2), RPARC(3,3) / 'WIND', 'VEL', 'VEL' //
DATA RPARC(4,1), RPARC(4,2), RPARC(4,3) / 'GRID', 'CUT', 'FENT' //
DATA RPARC(5,1), RPARC(5,2), RPARC(5,3) / 'VEID', 'CUT', 'FENT' //
DATA RPARC(6,1), RPARC(6,2), RPARC(6,3) / 'TIDE', 'LEV', 'VEL' //
C
C READ THE INFORMATION NEEDED FOR WRITE
C
WRITE(NW,447)
POPRAI('1' INPUT PARAMETERS')
C
CALL READ1( WPT, WNC, '1, 2)
CALL READ1( WU, WNU, '1, 4)
CALL READ1( WUM, WUP, '1, 900)
CALL READ1( NI, WNI, '1, 19)
CALL READ1( NUN, WNU, '1, 19)
CALL READ1( DC, WDC, '1, 19)
C
C READ IN GRID DEFINITIONS
C
CALL READ0(WC)
C
C TEST TO SEE IF THE TITLES ARE RIGHT
C
DO 60C I=1,6
IF (N1(1), EQ, RPARC(2,1), .AND. (N2(2), EQ, RPARC(1,2), .AND.
1  (N3(3), EQ, RPARC(1,3))) GO TO 60I
60C CONTINUE
WRITE(NW,60) BAR
C
69  FORMAT(21,' TITLES DO NOT MATCH', 3A4, ' READ IN')
60I STOP
60I CONTINUE
C
C DO LOOP OVER STEPS FOR COMPUTATIONS AND WRITING
C
DO 70 I=1, WOP
CALL FIZ(RK, ARAY1, ARAY2, RPAAT1, RPAAT2)
CALL ARAYO( WDIRA, NO, WOP, WDIR,
1  ARAY1, ARAY2, RPAAT1, RPAAT2)
TIME = TIME + DT
70 CONTINUE
STOP
END
SUBROUTINE READ0(WC)
C
C THIS READS FROM UNIT 5 ALL THE UNITS AND CONSTANTS
C
C .....
CORROD /DATA/ BAR(3), VAP1(2), NO, WUNIT, ISCAL,
1  VAR2(2), UNITS1(3), UNITS2(3), UNITS3(2),
2  IJAX, JMAX, ANGLE, XL, YL, XS, YS
C
C READ IN INFORMATION
CALL READ1( ISCAL, '1, 2)
CALL READ1( IJAX, '1, 30)
CALL READ1( JMAX, 'JMAX', '1, 30)
CALL READ1( ANGLE, 'ANGLE', '1)
CALL READ1( XS, 'XS', '1)
CALL READ1( YS, 'YS', '1)
CALL READ1( XL, 'XL', '1)
CALL READ1( YL, 'YL', '1)
CALL READ1( WU, 'WU', '1)
CALL READ1( WUM, 'WUM', '1)
CALL READ1( UNITS1, 'UNITS1', '1)
CALL READ1( UNITS2, 'UNITS2', '1)
CALL READ1( UNITS3, 'UNITS3', '1)
IF (NO, EQ, 1) STOP
CALL READ1( WPT, 'WPT', '1)
CALL READ1( UNITS2, 'UNITS2', '1)
RETURN
END
SUBROUTINE FIZ(RK, ARAY1, ARAY2, RPAAT1, RPAAT2)
C
C THIS SUBROUTINE PERFORMS THE NECESSARY STEPS TO
C READ THE DATA NEEDED FOR ARAYO
C
DIMENSION ARAY1(30,30), ARAY2(30,30), RPAAT1(30,30), RPAAT2(30,30)
CORROD /DATA/ BAR(3), VAP1(2), NO, WUNIT, ISCAL,
1  VAR2(2), UNITS1(3), UNITS2(3), UNITS3(2),
2  IJAX, JMAX, ANGLE, XL, YL, XS, YS
DATA ICT / 0 /
PI = 3.14159
SCAL = 6371.0*1000.0*PI/180.0
C
DO 800 I=1, IJAX
FORMAT(15F6.2)
READ(UNIT,500) (ARAY1(I,J), J=1, JMAX)
800 CONTINUE
DO 801 I=1, IJAX
READ(UNIT,500) (ARAY2(I,J), J=1, JMAX)

```

```

801 CONTINUE
C THIS SECTION CONVERTS THE ARAY FROM DEGREES/SEC TO
C DEGREES/SEC IF NEEDED.
IF (ISCAL, EQ, 1) RETURN
VLT = VL
NO 900 I=1, IJAX
DO 901 J=1, JMAX
ARAY1(I,J) = ARAY1(I,J) / SCAL * COS(VLAT / 57.296)
ARAY2(I,J) = ARAY2(I,J) / SCAL
VLT = VLT + VS
901 CONTINUE
900 CONTINUE
RETURN
END
SUBROUTINE ARAYO( WDIRA, NO, WOP, WDIR,
1  ARAY1, ARAY2, RPAAT1, RPAAT2)
C
C SUBROUTINE DESCRIPTION
C
C THIS SUBROUTINE READS IN ONE OF TWO ARAYS FOR THE VARIOUS
C GRID USED IN THE PROGRAM, SPECIFICALLY THE DEPTH GRID, THE
C GRID VELOCITY GRID, THE TEMPERATURE GRID AND THE SEA STATE
C GRID.
C
C VARIABLE DESCRIPTION
C
C SUBROUTINE ARGUMENTS
C
C (1) NO - FORMAT CONTROL: 1 - UNFORMATTED REAL;
C 2 - UNFORMATTED INTEGER;
C 3 - FORGOTTEN REAL;
C 4 - FORGOTTEN INTEGER.
C
C (3) NO - # OF ARAYS TO BE READ IN.
C (4) WDIR - DESCRIPTION FOR VARIABLE TO BE READ IN.
C (5) ARAY1 - FIRST ARAY READ IN.
C (6) ARAY2 - SECOND ARAY READ IN.
C (7) IJAX - # OF ELEMENTS IN X IN THE INPUT ARAYS.
C (8) JMAX - # OF ELEMENTS IN Y IN THE INPUT ARAYS.
C (9) ANGLE - ANGLE BETWEEN THE X AXIS FOR THE INPUT VARIABLES
C AND LINES OF CONSTANT LATITUDE.
C (10) XL - LONGITUDE OF THE ORIGIN OF THE FLOATING GRID.
C (11) YL - LATITUDE OF THE ORIGIN OF THE FLOATING GRID.
C (12) XS - GRID SPACING IN X.
C (13) YS - GRID SPACING IN Y.
C (14) RPAAT1 - EQUIVALENCED TO ARAY1 IN THE CALLING PROGRAM.
C (15) RPAAT2 - EQUIVALENCED TO ARAY2 IN THE CALLING PROGRAM.
C
C OTHER VARIABLES USED IN THE SUBROUTINE
C
C BAR - THE DESCRIPTOR OF THE INPUT VARIABLE STOPPED
C WITH THE DATA.
C VAP1 -2- NAME OF ARAY1 TO BE USED IN PRINTOUT HEADER.
C VAP2 -3- NAME OF ARAY2 TO BE USED IN PRINTOUT HEADER.
C UNITS1 -3- UNITS OF ARAY1 TO BE USED IN PRINTOUT HEADER.
C UNITS2 -3- UNITS OF ARAY2 TO BE USED IN PRINTOUT HEADER.
C
C NOTE 1: THE ARAYS ARAY1 AND ARAY2 ARE EQUIVALENCED IN THE
C MAIN PROGRAM TO THE ARAYS RPAAT1 AND RPAAT2. THE
C PARAMETER NO DETERMINES IF AN INTEGER OR A FLOATING
C POINT VALUE IS TO BE READ IN.
C
C .....
DIMENSION STATEMENTS
DIMENSION EX(15), ARAY1(30,30), ARAY2(30,30),
1  RPAAT1(30,30), RPAAT2(30,30)
DIMENSION ARAY1(30,30), ARAY2(30,30)
CORROD /DATA/ BAR(3), VAP1(2), NO, WUNIT, ISCAL,
1  VAR2(2), UNITS1(3), UNITS2(3), UNITS3(2),
2  IJAX, JMAX, ANGLE, XL, YL, XS, YS
C
C DATA STATEMENTS
DATA PI, NO, WPT / 3.14159, 6, 1/
DATA EX / 1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15/
DATA BAR1, BAR2 / 'DIRTY', 'VEID' /
C
C S T A R T H E R E
C
C DETERMINE DIMENSIONS OF GRIDS
C
C READ IN GRID DEFINITION VARIABLES (POPRAI'D).
C
IF (WU, LE, 2) GO TO 20
WRITE (NO,100) BAR, VAP1, UNITS1, VAR2, UNITS2
100 FORMAT(13A4)
WRITE (NO,105) IJAX, JMAX, ANGLE, XL, YL, XS, YS, UNITS3
105 FORMAT(215,3F10.4,2F10.2,2A4)
GO TO 25
C
C READ IN GRID DEFINITION VARIABLES (UNFORMATTED).
C
20 CONTINUE
WRITE (NO) BAR, VAP1, UNITS1, VAP2, UNITS2
WRITE (NO) IJAX, JMAX, ANGLE, XL, YL, XS, YS, UNITS3
C
CHECK THAT THIS IS THE DATA REQUESTED.
C
25 CONTINUE
IF (WPT) 10, 11, 12
C
WRITE GRID DEFINITION VARIABLES AND HEADER IF OUTPUT REQUESTED.
C
12 CONTINUE
WPT = TIME / 3600.0
WRITE (NO,200) BAR, WPT, WU, IJAX, XS, UNITS3, JMAX, YS, UNITS3
200 FORMAT('1',80I,3A4,' INPUT DATA ',F10.2,' HOURS AFTER',
1  ' THE BEGINNING OF THE SPILL',/A4,' THE ',JAX,
2  ' GRID HAS ', IS, ' DIVISIONS IN X SPACED ',G12.3,
3  ' 2A4,' APART/261,' AND ',YS,
4  ' DIVISIONS IN Y SPACED ',G12.3,2A4,' APART.'/)
WRITE (NO,210) BAR, XL, YL
210 FORMAT('1',THE (1,1) GRID LOCATION OF THE ',3A4,
1  ' COORDINATE SYSTEM IS BY ',
2  ' F10.6,' DEGREES LONGITUDE AND ',F10.6,
3  ' DEGREES LATITUDE./)
IF (ANGLE, NE, 0.0) WRITE (NO,215) BAR, ANGLE
215 FORMAT('1',FINALLY THE X AXIS OF THE ',3A4,

```

Figure VII.-1. GRIDS

```

1      * GRID BAREI AN ANGLE (COUNTERCLOCKWISE) OF P10.6,
2      * DEGREES WITH LINES OF /AI, 'CONSTANT LATITUDE.'
ANGLE = ANGLE * PI / 180.0
GO TO 10
C
C     HERE ONLY IF THE SHORT DIAGNOSTIC FORM IS DESIRED.
C
11     CONTINUE
WRITE (80,230) BAR, TIME
230    FORMAT('I, 'RES' .3A, ' INFORMATION IS BEING READ IN', P10.2,
1      ' SECONDS INTO THE SPILL')
C
C     HERE TO READ IN THE DATA.
C
10     CONTINUE
C
C     BRANCH TO READ DIFFERENT FORMAT TYPES.
C
GO TO (80,50,60,70), BU
C
C     HERE TO READ UNFORMATTED REAL VARIABLES.
C
40     CONTINUE
WRITE (80) ((ARAT1(I,J), I=1, IMAI), J=1, JRAI)
IF (80.EQ.1) GO TO 80
WRITE (80) ((ARAT2(I,J), I=1, IMAI), J=1, JRAI)
GO TO 80
C
C     HERE TO READ UNFORMATTED INTEGER VARIABLES.
C
50     CONTINUE
WRITE (80) ((IBAT1(I,J), I=1, IMAI), J=1, JRAI)
IF (80.EQ.1) GO TO 90
WRITE (80) ((IBAT2(I,J), I=1, IMAI), J=1, JRAI)
GO TO 90
C
C     HERE TO READ FORMATTED REAL VARIABLES.
C
60     CONTINUE
DO 62 J=1, JRAI
WRITE (80,110) ((ARAT1(I,J), I=1, IMAI)
110    FORMAT(10F4.2)
62     CONTINUE
IF (80.EQ.1) GO TO 80
DO 64 J=1, JRAI
WRITE (80,110) (ARAT2(I,J), I=1, IMAI)
64     CONTINUE
GO TO 80
C
C     HERE TO READ FORMATTED INTEGER VARIABLES.
C
70     CONTINUE
DO 72 J=1, JRAI
WRITE (80,120) ((IBAT1(I,J), I=1, IMAI)
120    FORMAT(10I4)
72     CONTINUE
IF (80.EQ.1) GO TO 90
DO 74 J=1, JRAI
WRITE (80,120) (IBAT2(I,J), I=1, IMAI)
74     CONTINUE
C
GO TO 90
C
C     HERE TO PRINT REAL ARRAYS.
C
80     CONTINUE
IF (80PTA.LE.0) RETURN
DC 96 I=1, IMAI
DO 96 J=1, JRAI
ARAT1(I,J) = ARAT1(I,J)
ARAT2(I,J) = ARAT2(I,J)
96     WRITE (*,*)
C
C     HERE TO SCALE VALUES FOR PRINTOUT IF ISCAL = 1
C
IF (ISCAL.EQ.1) GO TO 56
IF (80PT1.EQ.8471) GO TO 55
IF (80PT1.EQ.8482) GO TO 56
55     RPT = 0
WRITE (80,240)
240    FORMAT(2I, ' ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED',
1      ' BY 10 ** -6')
56     CONTINUE
IBAT1 = IBAT1
IF (IBAT1.GT.15) IBAT1 = 15
WRITE (80,220) VAP1, UNITS1, (RZ(II), II=1, IMAI)
220    FORMAT('/501.2A4, ' VALUES IF UNITS OF '3A//4, '1', 55)
1      ' ELEMENTS//11, 'ELEMENTS', 11, 15(2,61)//)
IF (RPT.NE.1) GO TO 77
DO 71 I=1, IMAI
DO 71 J=1, JRAI
ARAT1(I,J) = ARAT1(I,J) * (10**6.0)
77     CONTINUE
J = JRAI + 1
DO 82 R=1, JRAI
J = J - 1
WRITE (80,240) J, (ARAT1(I,J), I=1, IMAI)
240    FORMAT('0', 14, 51, 15CE.1/(81, 15CE.1))
82     CONTINUE
IF (80.EQ.1) RETURN
WRITE (80,220) VAP2, UNITS2, (RZ(II), II=1, IMAI)
IF (RPT.NE.1) GO TO 79
DO 76 I=1, IMAI
DO 76 J=1, JRAI
ARAT2(I,J) = ARAT2(I,J) * (10**6)
76     CONTINUE
J = JRAI + 1
DO 84 R=1, JRAI
J = J - 1
WRITE (80,240) J, (ARAT2(I,J), I=1, IMAI)
84     CONTINUE
RETURN
C
C     HERE TO PRINT INTEGER ARRAYS.
C
90     CONTINUE
IF (80PTA.LE.0) RETURN
IBAT1 = IBAT1
IF (IBAT1.GT.15) IBAT1 = 15
WRITE (80,220) IBAT1, UNITS1, (RZ(II), II=1, IMAI)
J = JRAI + 1

```

```

STOP
100    WRITE (80,30) I, IMAI
30     FORMAT(6I, 3A, 5I, 18)
RETURN
END
SUBROUTINE READP2(I, IMAI)
DIMENSION I(2)
REAL*8 IBAT1, IMAI
DATA BU, BU/5, 6/
READ (80,10) I, IMAI
10     FORMAT(7I, 2A, 5I, 18)
IF (IBAT1.EQ. IMAI) GO TO 100
WRITE (80,20) IMAI, IMAI
20     FORMAT(2I8 CARDS OUT OF ORDER, .A8, 6B READ, .A8, 10H FIGURES)
STOP
100    WRITE (80,30) I, IMAI
30     FORMAT(9I, 2A, 5I, 18)
RETURN
END
//GO.SISIZ DD *
1      EPITA
2      EC
1      BU
1      BUP
1      BE
5      PDAT
10800.0 DC
1      ISCAL
5      IMAI
5      JRAI
20.0   ANGLE
500.00 IE
800.00 VS
71.75  XI
39.75  TI
WIRE VEL TITLE
D      VAP1
E /SEC UNITS1
RETIE5 UNITS1
V      VAP2
E /SEC UNITS2
1.00 2.00 3.00 4.00 5.00
1.00 2.00 3.00 4.00 5.00
1.00 2.00 3.00 4.00 5.00
1.00 2.00 3.00 4.00 5.00
1.00 2.00 3.00 4.00 5.00
6.00 0.00 0.00 0.00 0.00
0.00 0.00 0.00 0.00 0.00
0.00 0.00 0.00 0.00 0.00
0.00 0.00 0.00 0.00 0.00
//GO.FT01P0C1 DE DUM*
//CC.FT02P0C1 DD DS=U81.E1A1.BUPPUS.CDISP=SHF
//CC.FT03P0C1 DD DS=U81.LC71.VINDOIL.KUPT,DISP=SHF
//

```

Figure VII.-1. GRIDS

```

//K12M478 JOB (R1A100,128,2.0), 'READ DATA ON DISK'
// EXEC PGM=DC, REGION=0, P1='STAGOUT(C,2019)'
// DD=READDATA(C,2019)
// UNIT=RD01
SUBROUTINE DESCRIPTION
THIS SUBROUTINE READS IN ONE OR TWO ARRAYS FOR THE VARIOUS
GRIDS USED IN THE PROGRAM, SPECIFICALLY THE DEPTH GRID, THE
GRID VELOCITY GRID, THE TEMPERATURE GRID AND THE SEA STATE
GRID.
VARIABLE DESCRIPTION
SUBROUTINE ARGUMENTS
(1) BU - FORMAT CONTROL: 1 - UNFORMATTED REAL;
2 - UNFORMATTED INTEGERS;
3 - FORMATTED REAL;
4 - FORMATTED INTEGER.
(2) BU - UNIT FROM WHICH DATA IS READ.
(3) BU - # OF ARRAYS TO BE READ IN.
(4) NAME - DESCRIPTOR FOR VARIABLE TO BE READ IN.
(5) ARRAY1 - FIRST ARRAY READ IN.
(6) ARRAY2 - SECOND ARRAY READ IN.
(7) IBA1 - # OF ELEMENTS IN X IN THE INPUT ARRAYS.
(8) IBA2 - # OF ELEMENTS IN Y IN THE INPUT ARRAYS.
(9) ANGLE - ANGLE BETWEEN THE X AXIS FOR THE INPUT VARIABLES
AND LINES OF CONSTANT LATITUDE.
(10) XL - LONGITUDE OF THE ORIGIN OF THE FLOATING GRID.
(11) YL - LATITUDE OF THE ORIGIN OF THE FLOATING GRID.
(12) XS - GRID SPACING IN X.
(13) YS - GRID SPACING IN Y.
(14) RARAT1 - EQUIVALENT TO ARRAY1 IN THE CALLING PROGRAM.
(15) RARAT2 - EQUIVALENT TO ARRAY2 IN THE CALLING PROGRAM.
OTHER VARIABLES USED IN THE SUBROUTINE
NAME - THE DESCRIPTOR OF THE INPUT VARIABLE STORED
WITH THE DATA.
VAR1 - 2 NAME OF ARRAY1 TO BE USED IN PRINTOUT HEADER.
VAR2 - 2 NAME OF ARRAY2 TO BE USED IN PRINTOUT HEADER.
UNITS1 - 3- UNITS OF ARRAY1 TO BE USED IN PRINTOUT HEADERS.
UNITS2 - 3- UNITS OF ARRAY2 TO BE USED IN PRINTOUT HEADERS.
NSTEP - NUMBER OF STEPS TO BE READ.
NOTE 1: THE ARRAYS ARRAY1 AND ARRAY2 ARE EQUIVALENT IN THE
DATA PROGRAM TO THE ARRAYS RARAT1 AND RARAT2. THE
PARAMETER NSTEP DESCRIBES IF AN INTEGER OR A FLOATING
POINT VALUE IS TO BE READ IN.
DISCUSSION STATEMENTS
DIMENSION ARRAY1( 30, 30), ARRAY2( 30, 30), VAR(3), UNITS(2)
DIMENSION VAR1(2), VAR2(2), UNITS1(3), UNITS2(3)
DIMENSION XL(15), ARRAY1( 30, 30), ARRAY2( 30, 30)
DIMENSION ARRAY1(30,30), ARRAY2(30,30)
DIMENSION NAME(8,3)
DATA STATEMENTS
DATA PI, BU / 3.14159, 4/
DATA XL / 1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15/
DATA VAR1, VAR2 / 'OTID', 'TID' /
DATA UNITS / 0, 0 /
DATA NAME(1,1), NAME(1,2), NAME(1,3) / 'BATH', 'TRET', 'PT' /
DATA NAME(2,1), NAME(2,2), NAME(2,3) / 'TEMP', 'FRAC', 'UPE' /
DATA NAME(3,1), NAME(3,2), NAME(3,3) / 'WIND', 'VEL', ' ' /
DATA NAME(4,1), NAME(4,2), NAME(4,3) / 'OTID', 'COR', 'HEAT' /
DATA NAME(5,1), NAME(5,2), NAME(5,3) / 'TID', 'COR', 'HEAT' /
DATA NAME(6,1), NAME(6,2), NAME(6,3) / 'TID', 'LEV', 'EL' /
S T A F F   I   B   E
WRITE(99,997)
997 FORMAT(' INPUT PARAMETERS')
CALL READI( 'BPRAT', 'BPRTA', 1, 1)
CALL READI( 'BU', 'BU', 1, 2)
CALL READI( 'NAME', 'NAME', 1, 3)
CALL READI( 'NSTEP', 'NSTEP', 1, 1)
CALL READI( 'SCALE', 'SCALE', 1, 2)
DO 999 I=1, NSTEP
DETERMINE DIMENSIONS OF GRIDS
READ IF GRID DEFINITION VARIABLES (FORMATTED).
IF (BU.EQ.2) GO TO 20
READ (BU,100) NAME, VAR1, UNITS1, VAR2, UNITS2
100 FORMAT('3A,100', NAME, VAR1, UNITS1, VAR2, UNITS2)
READ (BU,105) IBA1, IBA2, ANGLE, XL, YL, XS, YS, UNITS3
105 FORMAT('2I5,3F10.6,2F10.2,2A')
GO TO 25
READ IF GRID DEFINITION VARIABLES (UNFORMATTED).
20 CONTINUE
READ (BU) NAME, VAR1, UNITS1, VAR2, UNITS2
READ (BU) IBA1, IBA2, ANGLE, XL, YL, XS, YS, UNITS3
CONTINUE
TEST TO SEE IF THE TITLES ARE RIGHT
DO 400 I=1,6
IF (NAME(I).EQ.NAME(1,1)).AND.(NAME(2).EQ.NAME(1,2)).AND.
1 (NAME(3).EQ.NAME(2,3)) GO TO 601
400 CONTINUE
WRITE(99,69) NAME
69 FORMAT('21', ' TITLES DO NOT MATCH', 3A, ' READ IN')
STOP
401 CONTINUE
IF (BPRTA) 10, 11, 12
WRITE GRID DEFINITION VARIABLES AND HEADER IF OUTPUT REQUESTED.
12 CONTINUE

```

```

PRINT = TIME / 3600.0
WRITE (BU,200) NAME, VAR1, VAR2, IBA1, IBA2, UNITS1, UNITS2
200 FORMAT('1', '001,3A, ' INPUT DATA ', F10.2, ' GROUPS APPEAR')
1 ' THE BEGINNING OF THE SPILL '// '01', 'THE ', 3A,
2 ' GRID HAS ', 15, ' DIVISIONS IN X SPACED ', G12.3,
3 'APART', 'AND ', 15,
4 ' DIVISIONS IN Y SPACED ', G12.3, 'APART.'/)
WRITE (BU,210) NAME, XL, YL
210 FORMAT('1', 'THE (1,1) GRID LOCATION OF THE ', 3A,
1 ' CORRESPONDING SYSTEM IS AT ',
2 ' F10.6, ' DEGREES LONGITUDE AND ', F10.6,
3 ' DEGREES LATITUDE.'/)
IF (ANGLE.NE.0.0) WRITE (BU,215) NAME, ANGLE
215 FORMAT('1', 'FINALLY THE X AXIS OF THE ', 3A,
1 ' GRID MAKES AN ANGLE (CLOCKWISE) OF ', F10.6,
2 ' DEGREES WITH LINES OF 'CONSTANT LATITUDE.'/)
ANGLE = ANGLE * PI / 180.0
GO TO 10
C
HERE ONLY IF THE SHORT DIAGNOSTIC FORM IS DESIRED.
C
11 CONTINUE
WRITE (BU,230) NAME, TIME
230 FORMAT('1', 'REV ', 3A, ' INFORMATION IS BEING READ IN', F10.2,
1 ' SECONDS INTO THE SPILL')
C
HERE TO READ IN THE DATA.
C
10 CONTINUE
C
SEARCH FOR FEAR DIFFERENT FORMAT TYPES.
C
GO TO (40,50,60,70), BU
C
HERE TO READ UNFORMATTED REAL VARIABLES.
C
40 CONTINUE
READ (BU) ((ARRAY1(I,J), I=1, IBA1), J=1, IBA2)
IF (SC.EQ.1) GO TO 60
READ (BU) ((ARRAY2(I,J), I=1, IBA2), J=1, IBA2)
GO TO 80
C
HERE TO READ UNFORMATTED INTEGER VARIABLES.
C
50 CONTINUE
READ (BU) ((ARRAY1(I,J), I=1, IBA1), J=1, IBA2)
IF (SC.EQ.1) GO TO 90
READ (BU) ((ARRAY2(I,J), I=1, IBA2), J=1, IBA2)
GO TO 90
C
HERE TO READ FORMATTED REAL VARIABLES.
C
60 CONTINUE
DO 62 J=1, IBA2
READ (BU,110) (ARRAY1(I,J), I=1, IBA1)
110 FORMAT('10F6.2)
CONTINUE
IF (SC.EQ.1) GO TO 80
DO 64 J=1, IBA2
READ (BU,110) (ARRAY2(I,J), I=1, IBA2)
64 CONTINUE
GO TO 80
C
HERE TO READ FORMATTED INTEGER VARIABLES.
C
70 CONTINUE
DO 72 J=1, IBA2
READ (BU,120) (ARRAY1(I,J), I=1, IBA1)
120 FORMAT('30I4)
CONTINUE
IF (SC.EQ.1) GO TO 90
DO 74 J=1, IBA2
READ (BU,120) (ARRAY2(I,J), I=1, IBA2)
74 CONTINUE
GO TO 90
C
HERE TO PRINT REAL ARRAYS.
C
80 CONTINUE
IF (ARRAY1.EQ.0) GO TO 999
DO 96 I=1, IBA1
DO 96 J=1, IBA2
ARRAY1(I,J) = ARRAY1(I,J)
ARRAY2(I,J) = ARRAY2(I,J)
NPT = 0
C
IF (SCALE.EQ.2), SCALE THE VALUES FOR PRINTOUT.
C
IF (SCALE.EQ.1) GO TO 54
IF (NAME(1).EQ.NAME(1)) GO TO 55
IF (NAME(1).EQ.NAME(2)) GO TO 56
NPT = 1
WRITE(9, 824)
24 FORMAT('21', ' ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED',
1 ' BY 10** -6')
54 CONTINUE
C
IBAX1 = IBA1
IF (SCALE.EQ.15) IBAAX1 = 15
WRITE (BU,220) VAR1, UNITS1, VAR2, UNITS2, (NAME(I), I=1, IBAAX1)
220 FORMAT('1', '001,3A, ' VALUES IN UNITS OF ', 3A, '01', 'Y', 55X,
1 ' ' ELEMENTS', 'X', 'ELEMENTS', 'Y', 15(12,6X) /)
IF (NPT.NE.1) GO TO 77
DO 71 I=1, IBA1
DO 71 J=1, IBA2
71 ARRAY1(I,J) = ARRAY1(I,J) * (10**6)
77 CONTINUE
J = IBA1 + 1
DO 82 I=1, IBA1
J = J - 1
WRITE (BU,280) J, (ARRAY1(I,J), I=1, IBAAX1)
280 FORMAT('0', '14,5I,15(12,7.3) / (81,15(12,7.3)) /)
CONTINUE
IF (SC.EQ.1) GO TO 999
IF (NPT.NE.1) GO TO 79
DO 76 I=1, IBA1
DO 76 J=1, IBA2
76 ARRAY2(I,J) = ARRAY2(I,J) * (10**6.0)
79 CONTINUE
WRITE (BU,230) VAR2, UNITS2, (NAME(I), I=1, IBAAX1)

```

Figure VII. - 2. READATA


```

      J = JBAY + 1
      DO 94 K=1,JBAY
        J = J - 1
        WRITE (99,240) J, (BARAYZ(I,J),I=1,IBAY)
94    CONTINUE
      GO TO 999
C
C   HERE TO PRINT INTEGER ARRAYS.
C
90    CONTINUE
      IF (SPRYA.LE.0) GO TO 999
      IBAY = IBAY
      IF (IBAY.EQ.15) IBAY = 15
      WRITE (99,220) VAR1, UNITS1, (KZ(I),I=1,IBAY)
      J = JBAY + 1
      DO 92 K=1,JBAY
        J = J - 1
        WRITE (99,250) J, (BARAY1(I,J),I=1,IBAY)
250   FORMAT(1H,15,4L,100I1)
92    CONTINUE
      IF (NO.EQ.1) GO TO 999
      WRITE (99,220) VAR2, UNITS2, (KZ(I),I=1,IBAY)
      J = JBAY + 1
      DO 94 K=1,JBAY
        J = J - 1
        WRITE (99,250) J, (BARAY2(I,J),I=1,IBAY)
94    CONTINUE
      TIME = TIME + 06*00.0
999   CONTINUE
C
C   E N D   H E R E
C
STOP
END
SUBROUTINE READ1(I,ENAR1,NU)
  EXTERNAL ENAR1, ENAR1
  DATA N1,NU/5,6/
  READ (N1,10) I,X1,X2,X3
10  FORMAT(I15,5I,AB)
  IF (I>NNAR1) ENAR1 GO TO 100
  WRITE (99,20) ENAR1, I,X1,X2,X3
20  FORMAT(21H CAPDS OUT OF CDFZ ,A6,6B READ ,A8,10R IFQUESTED)
  STOP
100  CONTINUE
  IF (K1.EQ.NU) GO TO 200
  IF (I.GT.N1) ,AND. (I.LE.NU) GO TO 200
  WRITE (99,40) ENAR1, NU, ENAR1, I
40  FORMAT(14H THE LIMITS OF ,J1,5H ARE ,J5,4R TO ,J5,
  1 6H. BUT ,A6,16B WAS READ IN AS ,J5)
  STOP
200  CONTINUE
  WRITE (99,30) I, ENAR1
30  FORMAT(21,15,5I,AB)
  RETURN
END
//GO.SYSIS DD *
          1  SPRTA
          1  NO
          1  NO
          10  END
//
          1  NO
          2  ISCAL
//GO.FY01001 DD DSN=ORT.ERAT.ISCAL2.WDIR.DISP=SUB
//

```

Figure VII.-2. READATA

```

C
C      MODEL DESCRIPTION
C
C      THIS MODEL DOES THE BOOKKEEPING AS WELL AS THE PHYSICS
C      NECESSARY TO KEEP TRACK OF SPILLED OIL. THE ENVIRONMENT
C      IS DIVIDED UP INTO FIVE REGIONS - THE ATMOSPHERE - THE
C      WATER COLUMN - THE WATER SURFACE - THE BOTTOM - THE SHORE.
C      NOTE: SOME SUBROUTINES MAY ONLY BE USED SUBROUTINES AND
C      PERFORM NO FUNCTION AT THIS TIME ALL PROCESSES
C      ARE NOT FULLY UNDERSTOOD SO SPACE HAS BEEN LEFT
C      SO THAT THESE MAY BE ADDED LATER.
C
C      EVERYTHING IS REFERENCED TO THE DEPTH GRID (IE. THE PARTICLES
C      AND THE SPILLETS).
C      THE INTEGER VARIABLE ISCAL TELLS THE PROGRAM WHETHER THE
C      SPILL AREA COVERS A LARGE ENOUGH FOR ERRORS IN CORRECTING
C      DEGREES TO METERS OF THIS SPILL. IF ISCAL=1, THEN THE
C      PROGRAM DOES THE CALCULATIONS IN METERS, OTHERWISE THE
C      CALCULATIONS ARE DONE IN DEGREES. IF ISCAL=2 THEN THE
C      PROGRAM WILL ONLY ACCEPT DATA IN DEGREES AND WITH NO
C      ANGLE WITH RESPECT TO LINES OF CONSTANT LATITUDE. THE
C      CALCULATIONS CONCERNING DEPTH (IE. CONCENTRATION) ARE
C      ALWAYS DONE IN METERS (IE THE DEPTH IS BEING CONVERTED
C      TO ANY OTHER DIMENSION). THE FLOATING GRID ALWAYS HAS
C      THE SAME ORIENTATION AS THE DEPTH GRID (IE. THE ANGLE
C      OF THE FLOATING GRID WITH RESPECT TO LINES OF
C      CONSTANT LATITUDE IS THE SAME AS THE DEPTH GRID).
C
C      MODEL VARIABLES
C
C      CHEMICAL TREATMENT: CHEM
C
C      LCHM - # OF CHEM TREATMENT EFFORTS BEGUN DURING THIS STEP.
C      NCHM - # OF CHEM TREATMENT EFFORTS BEING ADDED LATER.
C      NCHL - UNIT FROM WHICH THE TREATMENT DATA SHALL BE READ.
C      NCHRE - NUMBER TIME THIS TREATMENT EFFORT BEGINS (SECS).
C      DCHRM - NUMBER DURATION OF TREATMENT EFFORT (SECS).
C      RCHMA - RADIUS OF TREATED AREA (METERS).
C      RCHMB - RADIUS OF TREATED AREA (DEGREES).
C      TCHME - INITIAL TEMPERATURE OF TREATED OIL (DEGREES/CM).
C      TCHMF - TEMPERATURE OF TREATED OIL (DEGREES/CM).
C      VCHME - VOLUME OF DISPERSANT USED PER BOG (LITERS/BOG).
C      VCHMF - VOLUME OF DISPERSANT USED PER SQ. METER (LITERS/METER**2).
C      XCHME - CENTER OF TREATED AREA (LONGITUDE).
C      XCHMF - CENTER OF TREATED AREA (LATITUDE).
C      PCHEM - PERCENTAGE OF OIL REMAINING AT THE TREATED
C      AREA BEYOND THE SPILL AREA
C
C      PHYSICAL CLEANUP: CLEW
C
C      LCLE - # OF CLEANUP EFFORTS BEGUN DURING THIS TIME STEP.
C      NCLE - # OF CLEANUP EFFORTS AFTER ADDING LATER.
C      NCLD - UNIT FROM WHICH THE CLEANUP EFFORT DATA SHALL BE READ.
C      NCLRE - BEGINNING TIME OF THIS CLEANUP EFFORT (SECS).
C      DCLRM - DURATION OF THIS CLEANUP EFFORT (SECS).
C      RCLMA - RADIUS OF THIS CLEANUP EFFORT (M).
C      RCLMB - RADIUS OF THIS CLEANUP EFFORT (DEGREES).
C      VCLM - OIL RECOVERY RATE (TONS/BOG).
C      XCLM - CENTER OF THIS EFFORT (LONGITUDE).
C      YCLM - CENTER OF THIS EFFORT (LATITUDE).
C
C      COMPUTATIONAL CELL GRID DEFINITION: CORP
C
C      NAC1 - # OF GRID ELEMENTS IN X FOR THE COMPUTATIONAL GRID.
C      NAC2 - # OF GRID ELEMENTS IN Y FOR THE COMPUTATIONAL GRID.
C      NCD - UNIT FROM WHICH THE COMPUTATIONAL DATA SHALL BE READ.
C      NCO - FORMAT CONTROL: 1 - UNFORMATTED REAL;
C      2 - UNFORMATTED INTEGER;
C      3 - FORMATTED REAL;
C      4 - FORMATTED INTEGER.
C
C      AC - ANGLE BETWEEN THE X AXIS OF THE COMPUTATIONAL
C      GRID AND LINES OF CONSTANT LATITUDE (DEGREES).
C      NCOBP - NAC1, NAC2 - COMPUTATIONAL CELL DEFINITION.
C      XCL - LONGITUDE OF THE ORIGIN OF THE COMPUTATIONAL GRID.
C      YCL - LATITUDE OF THE ORIGIN OF THE COMPUTATIONAL GRID.
C      XCS - GRID SPACING IN X OF THE COMPUTATIONAL GRID (METERS).
C      YCS - GRID SPACING IN Y OF THE COMPUTATIONAL GRID (METERS).
C
C      WATER DEPTH GRID: DPTH
C
C      NAD1 - # OF GRID ELEMENTS IN X FOR THE DEPTH GRID.
C      NAD2 - # OF GRID ELEMENTS IN Y FOR THE DEPTH GRID.
C      NDD - UNIT FROM WHICH THE DEPTH DATA SHALL BE READ.
C      NDO - FORMAT CONTROL (SEE NCO).
C      AD - ANGLE BETWEEN THE X AXIS OF THE DEPTH GRID AND
C      LINES OF CONSTANT LATITUDE (DEGREES).
C      DPTHG - NAD1, NAD2 - DEPTH OF OCEAN AT EACH ELEMENT (METERS).
C      XDL - LONGITUDE OF THE ORIGIN OF THE DEPTH GRID.
C      YDL - LATITUDE OF THE ORIGIN OF THE DEPTH GRID.
C      XDS - GRID SPACING IN X OF THE DEPTH GRID (METERS).
C      YDS - GRID SPACING IN Y OF THE DEPTH GRID (METERS).
C
C      TIDAL ELEVATION: ELVE
C
C      NAE1 - # OF GRID ELEMENTS IN X FOR THE TIDAL ELEVATION GRID.
C      NAE2 - # OF GRID ELEMENTS IN Y FOR THE TIDAL ELEVATION GRID.
C      NED - UNIT FROM WHICH THE TIDAL ELEVATION DATA SHALL BE READ.
C      NED - FORMAT CONTROL (SEE NDO).
C      AE - ANGLE BETWEEN THE X AXIS OF THE TIDAL ELEVATION GRID
C      AND LINES OF CONSTANT LATITUDE.
C      NGET - NAE1, NAE2 - ELEVATION OF SEA LEVEL DUE TO TIDE AT
C      EACH GRID POINT (METERS).
C      XEL - LONGITUDE OF ORIGIN OF TIDAL ELEVATION GRID.
C      YEL - LATITUDE OF ORIGIN OF TIDAL ELEVATION GRID.
C      XES - GRID SPACING IN X OF THE TIDAL ELEVATION GRID (METERS).
C      YES - GRID SPACING IN Y OF THE TIDAL ELEVATION GRID (METERS).
C
C      3-D FLOATING CURRENT GRID: FLOT
C
C      NAF1 - # OF GRID ELEMENTS IN X FOR THE FLOATING CURRENT GRID.
C      NAF2 - # OF GRID ELEMENTS IN Y FOR THE FLOATING CURRENT GRID.
C      NAF3 - # OF GRID ELEMENTS IN Z FOR THE FLOATING CURRENT GRID.
C      NFD - UNIT FROM WHICH FLOATING CURRENT DATA SHALL BE READ.
C      NFO - FORMAT CONTROL (SEE NCO).
C      FV - 1 IF FLOATING CURRENTS ARE TO BE UPDATED THIS STEP,
C      0 OTHERWISE.
C      AP - ANGLE BETWEEN THE X AXIS OF THE FLOATING CURRENT GRID
C      AND LINES OF CONSTANT LATITUDE (DEGREES).
C      NAF1X, NAF1Y, NAF1Z - X COMPONENT OF CURRENT (M/SEC).
C      NAF2X, NAF2Y, NAF2Z - Y COMPONENT OF CURRENT (M/SEC).
C      NAF3X, NAF3Y, NAF3Z - Z COMPONENT OF CURRENT (M/SEC).
C
C      EPL - LONGITUDE OF THE ORIGIN OF THE FLOATING CURRENT GRID.
C      EPL - LATITUDE OF THE ORIGIN OF THE FLOATING CURRENT GRID.
C      EPL - DISTANCE BELOW SEA LEVEL OF THE ORIGIN OF THE
C      FLOATING CURRENT GRID (METERS).
C      OF - 1000 IF THE FLOATING GRID IS VARIABLE TO THE BOTTOM.
C      EFS - GRID SPACING IN X OF THE FLOATING CURRENT GRID (METERS).
C      EFS - GRID SPACING IN Y OF THE FLOATING CURRENT GRID (METERS).
C      EFS - GRID SPACING IN Z OF THE FLOATING CURRENT GRID (METERS).
C      OF - 1000 IF THE GRID SPACING IS VARIABLE.
C
C      MISCELLANEOUS: CTRL
C
C      INSUB - # OF GRID ELEMENTS IN X OF THE SUBSURFACE GRID.
C      JNSUB - # OF GRID ELEMENTS IN Y OF THE SUBSURFACE GRID.
C      KNSUB - # OF GRID ELEMENTS IN Z OF THE SUBSURFACE GRID.
C      NPRTA - PRINT CONTROL: 0 - NO DIAGNOSTIC PRINTOUT;
C      1 - FULL DIAGNOSTIC PRINTOUT.
C      NPRTC - 1 - PRINT OUT CURRENT CLEANUP AND TREATMENT EFFORTS AND
C      SPILLER CHARACTERISTICS FOR EVERY TIME STEP.
C      0 - PRINT OUT ONLY WHEN BEG EFFORTS ARE STARTED OR
C      NEW SPILLETS APPEAR.
C      NR - INPUT FILE FOR STEP CONTROL PARAMETERS.
C      D1 - TIME STEP USED IN FOLLOWING THE SPILL (SECS).
C      SCALE - # OF METERS PER DEGREE LATITUDE.
C      WIDE - TIME SINCE THE BOG BEGAN (SECS).
C      TIMEAR - TIME AT WHICH THIS BOG IS TO END (SECS).
C      NBSPL - NUMBER OF SPILLER SPILLETS.
C      INSPAR - NUMBER OF BOGS TO BE REPRESENTED BY EACH PARTICLE
C      NDRCL - NUMBER OF PARTICLE CLASSES.
C      NSOEN - INTERVAL CONTROL PARAMETERS FOR SWITCHING TO
C      RESTART DATA SET.
C      NBOV - 1 THIS INDICATES A SHORT PREVIEW BOG
C      0 THIS INDICATES A FULL BOG. BOG
C      NSTPB - 0 THIS IS A RESTARTED BOG AND BOG DATA SETS
C      ARE TO BE USED FOR INPUT AND OUTPUT.
C      1 THIS INDICATES BOG WILL CONTINUE SWITCHING TO THE
C      SAME OUTPUT DATA SETS AS THE PREVIOUS BOG.
C
C      OUTPUT FILE NUMBERS
C
C      BOSP - SPILLER OUTPUT FILE.
C      BOPS - RESTART OUTPUT FILE.
C      BOCN - CONCENTRATION PARAMETERS OUTPUT FILE.
C      BOPM - PARTICLE PARAMETERS OUTPUT FILE.
C      BOVL - FLOATING GRID VELOCITIES OUTPUT FILE.
C      BOWS - BOGS BALANCE OUTPUT FILE.
C      BOPF - PARTICLES DEPOSITED ON BOTTOM OUTPUT FILE.
C      BOLT - PARTICLES LOST THROUGH OPEN BOUNDARIES
C      OUTPUT FILE.
C
C      DESCRIPTION OF INPUT VARIABLES
C
C      I N T E R A S
C
C      NPA1 - NUMBER OF PARTICLES.
C      NPA2 - 1 REPAID AND TRANSLATE FLOATING GRID
C      0 NO REPAID
C      PRINT INTERVAL PARAMETERS
C      NPRT - PRINT PARTICLE POSITION
C
C      EPRC - PRINT CONCENTRATION.
C      EPRV - PRINT VELOCITY VECTOR.
C      NCBIT - NUMBER OF PARTICLES BEING DEPOSED
C      CALCULATING CONCENTRATION.
C      NDIFF - 0 CONSTANT DIFFUSION COEFFICIENTS
C      1 SCALE DEPENDENT DIFFUSION COEFFICIENTS
C      NDISP - PRINT INTERVAL CONTROL FOR DISP
C      NPAC - PRINT PARTICLE PARAMETERS
C      NPEV - PRINT CONCENTRATION PARAMETERS
C      NPOE - PRINT VELOCITY VECTOR
C      NPOE - 0 PARTICLE DIFFUSION WITH SPREADING TRANSLATING GRID
C      1 ANALYTIC DIFFUSION WITH SPREADING TRANSLATING GRID
C      NSTRAN - 0 NO X TRANSPORTATION
C      1 X TRANSPORTATION
C      NPSRDS - INTERVAL PRINT CONTROL FOR BOGS BALANCE OUTPUT
C      NPSRSD - INTERVAL PRINT CONTROL FOR BOGS BALANCE INFORMATION
C      PRINTOUT (FLOATING GRID AND VARIABLE DIFFUSION).
C
C      B E A L V A R I A B L E S
C
C      DT - TIME STEP (SECS).
C      DE, DF, DE - GRID SPACING OF FLOATING GRID (FT).
C      DEI, DEI, DEI - TURBULENCE DIFFUSION COEFFICIENTS (FT**2/SEC).
C      EIL, EII - COEFFICIENTS USED IN SCALE DEPENDENT DIFFUSION.
C      NPOE, NPOE - POEAS USED IN SCALE DEPENDENT DIFFUSION.
C      RADIUS - RADIUS OF INITIAL UNIFORM PARTICLE DISTRIBUTION
C      AVERAGED OVER ONE TIDAL CYCLE
C      XG, YG - CENTER OF UNIFORM DISTRIBUTION IN THE PIREX
C      SYSTEM (GRID UNITS).
C      XGIC, YGIC - ORIGIN OF FLOATING SYSTEM IN PIREX SYSTEM (GRID UNITS).
C      XGIC - ORIGIN OF FLOATING GRID IN GRID UNITS FROM BOTTOM.
C      XGIC - VELOCITY ORIGIN OF INITIAL PARTICLE DISTRIBUTION.
C      NDISP - MINIMUM DURATION OF ENTRAPMENT.
C      NENT - MINIMUM DURATION OF ENTRAPMENT.
C      TRASS - MASS ESTABLISHED PER STEP.
C      APAC - DETERMINES THE FRACTION OF PARTICLES WITHIN BO
C      NBPAC - DETERMINES RADIUS WHEN PARTICLE DENSITY IS
C      NBPAC - DETERMINES RADIUS WHEN PARTICLE DENSITY IS
C      NBPAC - FACTOR WHICH DETERMINES RATE AT WHICH
C      PARTICLE DISTRIBUTION FALLS OFF.
C      NPAI - (RSPILL*(1.0-(ENT/5.0))/(BOFRAC*(ENT**1.4)),
C      COBB - RATIO OF DISTANCE BETWEEN SPILLETS WHICH WILL
C      CAUSE THEM TO COMBINE.
C      NDIAPRT - DIAPARTS OF PARTICLES.
C      NDIAPRT - SETTLING VELOCITY OF PARTICLES
C      PARTICLES WHICH ARE TREATED.
C
C      MASS BALANCE: MASS
C
C      NMA1 - MASS OF OIL LOST TO THE ATMOSPHERE (TONS).
C      NMA2 - MASS OF OIL BIOLOGICALLY COMBUSTED (TONS).
C      NMA3 - MASS OF OIL CLEANED UP (TONS).
C      NMA4 - MASS OF OIL WHICH WAS SETTLED TO THE BOTTOM (TONS).
C      NMA5 - MASS OF OIL SPILLED THROUGH PAI (TONS).
C      NMA6 - MASS OF OIL WHICH LEAVES THE STUDY AREA (TONS).
C      NMA7 - MASS OF OIL DEPOSITED ON THE SHORELINE (TONS).
C      NMA8 - MASS OF OIL IN SPILLETS ON THE SURFACE (TONS).
C      NMA9 - MASS OF OIL UNSPENDED IN THE WATER COLUMN (TONS).

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Figure VII.-3. MAIN

SEA STATE GRID: SEAS

BASIS - # OF GRID ELEMENTS IN X FOR THE SEA STATE GRID.
 BAIS1 - # OF GRID ELEMENTS IN Y FOR THE SEA STATE GRID.
 BSD - UNIT FROM WHICH SEA STATE DATA SHALL BE READ.
 BSU - POINT CONTROL (SEE SCU).
 BS - 1 IF SEA STATE VALUES ARE TO BE UPDATED THIS STEP
 0 OTHERWISE.
 AS - ANGLE BETWEEN THE X AXIS OF THE SEA STATE GRID AND
 LINES OF CONSTANT LATITUDE (DEGREES).
 WAVSCT -WAVELENGTH- WAVE AMPLITUDE (METERS).
 WAVPD -WAVE PERIOD- WAVE PERIOD (SEC).
 ZSL - LONGITUDE OF THE ORIGIN OF THE SEA STATE GRID.
 ZSL - LATITUDE OF THE ORIGIN OF THE SEA STATE GRID.
 ZSS - GRID SPACING IN X OF THE SEA STATE GRID (METERS).
 ZSS - GRID SPACING IN Y OF THE SEA STATE GRID (METERS).

SHORELINE DEFINITION: SHOR

BSRD - UNIT FROM WHICH SHORELINE DATA SHALL BE READ.
 BSROB - # OF POINTS USED TO DEFINE THE SHORELINE
 ZSHOR -SHOR- SHORELINE POINT (LONGITUDE).
 ZSHOB -SHOR- SHORELINE POINT (LATITUDE).

SPILL DEFINITION: SPIL

LSPIL - # OF SPILLETTS ADDED EXTERNALLY THIS STEP.
 BSPIL - # OF CLASSES OF OIL TO BE CONSIDERED.
 BSPD - UNIT FROM WHICH SPILLET DATA SHALL BE READ.
 BSPIL - # OF ACTIVE SPILLETTS AFTER ADDING LSPIL.
 BSPIL -SPIL- AREA OF SPILLET: FRACTION FODS FAT (METERS**2),
 THIS PARAMETER IS NEGATIVE IF VANTOIN:
 OF THIS SPILLET IS COMPLETE.
 BSPIL -SPIL- TIME SINCE THE SPILLET FIRST APPEARED.
 - ENTERED IN HOURS, CONVERTED TO SECONDS (SEC)
 DSPIL -SPIL- DENSITY OF OIL (GM/CM3).
 FSPIL -SPIL- FRACTION BY VOLUME OF SPIL TREATED.
 GSPIL -SPIL,SPIL- FRACTION BY MASS OF EACH CLASS OF OIL.
 RSPIL -SPIL- RADIUS OF SPILLET (METERS).
 ISPIL -SPIL- INTERFACIAL TENSION OF THE OIL (DYNES/CM).
 MSPIL -SPIL- THERMAL EXPANSION OF THE TREATAL FRACTION OF
 THE SPILLET (DYNES/CM).
 TSPIL -SPIL- DENSITY OF OIL AT TREF=0.
 TSPIL -SPIL- TOXICITY OF THE TREATED FRACTION OF THE SPILLET.
 VSPIL -SPIL- KINEMATIC VISCOSITY OF THE OIL (CENTISTOAKES).
 WSPIL -SPIL- MASS OF THE OIL IN THE SPILLET (TONS).
 XSPIL -SPIL- CENTER OF THE SPILLET (LONGITUDE).
 YSPIL -SPIL- CENTER OF THE SPILLET (LATITUDE).

TIDAL CURRENT 2-D PILED GRID: TIDI

THESE ARE TWO TIDAL GRIDS. IT IS ASSUMED THAT THEY HAVE THE
 SAME SPACING AND ORIENTATION. THE ORIGINS ARE DIFFERENT SO
 THAT THEY CAN BE OFFSET IF A SPACE STAGGERED BOUCHELL TIDAL
 IS USED

BASIS - # OF GRID ELEMENTS IN X FOR THE TIDAL CURRENT GRID.
 BAIS1 - # OF GRID ELEMENTS IN Y FOR THE TIDAL CURRENT GRID.
 BSD - UNIT FROM WHICH THE TIDAL CURRENT SHALL BE READ.
 BSU - POINT CONTROL (SEE SCU).

BS - 1 IF TIDAL VELOCITY VALUES ARE TO BE UPDATED THIS STEP
 0 OTHERWISE

AT - ANGLE BETWEEN THE X AXIS OF THE TIDAL CURRENT
 GRID AND LINES OF CONSTANT LATITUDE (DEGREES).
 UT -WAVELENGTH- U COMPONENT OF THE TIDAL CURRENT (M/SEC).
 VT -WAVELENGTH- V COMPONENT OF THE TIDAL CURRENT (M/SEC).
 ZTL0 - LONGITUDE OF THE ORIGIN OF THE 1-DIM TIDAL CURRENT GRID.
 ZTL1 - LONGITUDE OF THE ORIGIN OF THE 2-DIM TIDAL CURRENT GRID.
 ZTL2 - LONGITUDE OF THE ORIGIN OF THE 3-DIM TIDAL CURRENT GRID.
 ZTL3 - LONGITUDE OF THE ORIGIN OF THE 4-DIM TIDAL CURRENT GRID.
 ZTL4 - LONGITUDE OF THE ORIGIN OF THE 5-DIM TIDAL CURRENT GRID.
 ZTL5 - LONGITUDE OF THE ORIGIN OF THE 6-DIM TIDAL CURRENT GRID.
 ZTL6 - LONGITUDE OF THE ORIGIN OF THE 7-DIM TIDAL CURRENT GRID.
 ZTL7 - LONGITUDE OF THE ORIGIN OF THE 8-DIM TIDAL CURRENT GRID.
 ZTL8 - LONGITUDE OF THE ORIGIN OF THE 9-DIM TIDAL CURRENT GRID.
 ZTL9 - LONGITUDE OF THE ORIGIN OF THE 10-DIM TIDAL CURRENT GRID.
 ZTL0 - LONGITUDE OF THE ORIGIN OF THE 11-DIM TIDAL CURRENT GRID.
 ZTL1 - LONGITUDE OF THE ORIGIN OF THE 12-DIM TIDAL CURRENT GRID.
 ZTL2 - LONGITUDE OF THE ORIGIN OF THE 13-DIM TIDAL CURRENT GRID.
 ZTL3 - LONGITUDE OF THE ORIGIN OF THE 14-DIM TIDAL CURRENT GRID.
 ZTL4 - LONGITUDE OF THE ORIGIN OF THE 15-DIM TIDAL CURRENT GRID.
 ZTL5 - LONGITUDE OF THE ORIGIN OF THE 16-DIM TIDAL CURRENT GRID.
 ZTL6 - LONGITUDE OF THE ORIGIN OF THE 17-DIM TIDAL CURRENT GRID.
 ZTL7 - LONGITUDE OF THE ORIGIN OF THE 18-DIM TIDAL CURRENT GRID.
 ZTL8 - LONGITUDE OF THE ORIGIN OF THE 19-DIM TIDAL CURRENT GRID.
 ZTL9 - LONGITUDE OF THE ORIGIN OF THE 20-DIM TIDAL CURRENT GRID.
 ZTL0 - LONGITUDE OF THE ORIGIN OF THE 21-DIM TIDAL CURRENT GRID.
 ZTL1 - LONGITUDE OF THE ORIGIN OF THE 22-DIM TIDAL CURRENT GRID.
 ZTL2 - LONGITUDE OF THE ORIGIN OF THE 23-DIM TIDAL CURRENT GRID.
 ZTL3 - LONGITUDE OF THE ORIGIN OF THE 24-DIM TIDAL CURRENT GRID.
 ZTL4 - LONGITUDE OF THE ORIGIN OF THE 25-DIM TIDAL CURRENT GRID.
 ZTL5 - LONGITUDE OF THE ORIGIN OF THE 26-DIM TIDAL CURRENT GRID.
 ZTL6 - LONGITUDE OF THE ORIGIN OF THE 27-DIM TIDAL CURRENT GRID.
 ZTL7 - LONGITUDE OF THE ORIGIN OF THE 28-DIM TIDAL CURRENT GRID.
 ZTL8 - LONGITUDE OF THE ORIGIN OF THE 29-DIM TIDAL CURRENT GRID.
 ZTL9 - LONGITUDE OF THE ORIGIN OF THE 30-DIM TIDAL CURRENT GRID.
 ZTL0 - LONGITUDE OF THE ORIGIN OF THE 31-DIM TIDAL CURRENT GRID.
 ZTL1 - LONGITUDE OF THE ORIGIN OF THE 32-DIM TIDAL CURRENT GRID.
 ZTL2 - LONGITUDE OF THE ORIGIN OF THE 33-DIM TIDAL CURRENT GRID.
 ZTL3 - LONGITUDE OF THE ORIGIN OF THE 34-DIM TIDAL CURRENT GRID.
 ZTL4 - LONGITUDE OF THE ORIGIN OF THE 35-DIM TIDAL CURRENT GRID.
 ZTL5 - LONGITUDE OF THE ORIGIN OF THE 36-DIM TIDAL CURRENT GRID.
 ZTL6 - LONGITUDE OF THE ORIGIN OF THE 37-DIM TIDAL CURRENT GRID.
 ZTL7 - LONGITUDE OF THE ORIGIN OF THE 38-DIM TIDAL CURRENT GRID.
 ZTL8 - LONGITUDE OF THE ORIGIN OF THE 39-DIM TIDAL CURRENT GRID.
 ZTL9 - LONGITUDE OF THE ORIGIN OF THE 40-DIM TIDAL CURRENT GRID.
 ZTL0 - LONGITUDE OF THE ORIGIN OF THE 41-DIM TIDAL CURRENT GRID.
 ZTL1 - LONGITUDE OF THE ORIGIN OF THE 42-DIM TIDAL CURRENT GRID.
 ZTL2 - LONGITUDE OF THE ORIGIN OF THE 43-DIM TIDAL CURRENT GRID.
 ZTL3 - LONGITUDE OF THE ORIGIN OF THE 44-DIM TIDAL CURRENT GRID.
 ZTL4 - LONGITUDE OF THE ORIGIN OF THE 45-DIM TIDAL CURRENT GRID.
 ZTL5 - LONGITUDE OF THE ORIGIN OF THE 46-DIM TIDAL CURRENT GRID.
 ZTL6 - LONGITUDE OF THE ORIGIN OF THE 47-DIM TIDAL CURRENT GRID.
 ZTL7 - LONGITUDE OF THE ORIGIN OF THE 48-DIM TIDAL CURRENT GRID.
 ZTL8 - LONGITUDE OF THE ORIGIN OF THE 49-DIM TIDAL CURRENT GRID.
 ZTL9 - LONGITUDE OF THE ORIGIN OF THE 50-DIM TIDAL CURRENT GRID.

TEMPERATURE GRID: TRPC

BASIS - # OF GRID ELEMENTS IN X FOR THE TRPC GRID.
 BASIS1 - # OF GRID ELEMENTS IN Y FOR THE TRPC GRID.
 BSD - UNIT FROM WHICH TEMPERATURE DATA SHALL BE READ.
 BSU - POINT CONTROL (SEE SCU).
 BS - 1 IF TEMPERATURE VALUES ARE TO BE UPDATED THIS STEP,
 0 OTHERWISE.
 AS - ANGLE BETWEEN THE X AXIS OF THE TRPC GRID AND
 LINES OF CONSTANT LATITUDE (DEGREES).
 TR -WAVELENGTH- U COMPONENT OF THE TRPC (M/SEC).
 TR -WAVELENGTH- V COMPONENT OF THE TRPC (M/SEC).
 ZTL - LONGITUDE OF THE ORIGIN OF THE TEMPERATURE GRID.
 ZSL - LATITUDE OF THE ORIGIN OF THE TEMPERATURE GRID.
 ZSS - GRID SPACING IN X OF THE TRPC GRID (METERS).
 ZSS - GRID SPACING IN Y OF THE TRPC GRID (METERS).

WIND GRID: WIND

BASIS - # OF GRID ELEMENTS IN X FOR THE WIND GRID.
 BASIS1 - # OF GRID ELEMENTS IN Y FOR THE WIND GRID.
 BSD - UNIT FROM WHICH WIND DATA SHALL BE READ.
 BSU - POINT CONTROL (SEE SCU).
 BS - 1 IF WIND VALUES ARE TO BE UPDATED THIS STEP,
 0 OTHERWISE.
 AW - ANGLE BETWEEN THE X AXIS OF THE WIND GRID AND LINES
 OF CONSTANT LATITUDE (DEGREES).
 U -WAVELENGTH- U COMPONENT OF THE WIND (M/SEC).
 V -WAVELENGTH- V COMPONENT OF THE WIND (M/SEC).
 ZTL - LONGITUDE OF THE ORIGIN OF THE WIND VELOCITY GRID.
 ZSL - LATITUDE OF THE ORIGIN OF THE WIND VELOCITY GRID.
 ZSS - GRID SPACING IN X OF THE WIND GRID (METERS).
 ZSS - GRID SPACING IN Y OF THE WIND GRID (METERS).

NOTE 1: IN THE CALL TO ARAVIN THE FLOATING POINT ARRAY IS
 EQUIVALENT TO A PILED POINT ARRAY THUS ALLOWING
 THE SUBROUTINE TO READ IN EITHER A FLOATING POINT
 OR A PILED POINT ARRAY DEPENDING ON THE VALUE OF
 THE POINT CONTROL PARAMETERS.

VCLB(10), SCLE(10), YCLB(10)
 COMMON /DEPS/ DEP(8)
 COMMON /DEPOS/ DEPOS, BDEP
 COMMON /CORP/ CORP, BAI1, BAI2, AC, BCOBP(30,30), ECL, FCL,
 1 ECS, YCS
 COMMON /DPTR/ BAI1D, BAI2D, AD, DEPT(30,30), IDL, YDL,
 1 IDS, YDS
 COMMON /ELVE/ BAI1E, BAI2E, AE, BCOBP(30,30), EEL, YEL,
 1 EES, YES
 COMMON /FLAT/ BAI1F, BAI2F, BAI3F, BAI4F, AF, BPLT(15,15,10),
 1 BPLT(15,15,10), BPLT(15,15,10), BPLT(15,15,10), BPLT(15,15,10),
 COMMON /CMTL/ BAI1C, BAI2C, BAI3C, BAI4C, BAI5C, BAI6C, BAI7C,
 1 BAI8C, BAI9C, BAI10C, BAI11C, BAI12C, BAI13C, BAI14C, BAI15C,
 COMMON /BASS/ BAI1B, BAI2B, BAI3B, BAI4B, BAI5B, BAI6B, BAI7B,
 1 BAI8B, BAI9B, BAI10B, BAI11B, BAI12B, BAI13B, BAI14B, BAI15B,
 COMMON /ODTP/ BAI1D, BAI2D, BAI3D, BAI4D, BAI5D, BAI6D, BAI7D,
 1 BAI8D, BAI9D, BAI10D, BAI11D, BAI12D, BAI13D, BAI14D, BAI15D,
 1 BAI16D, BAI17D, BAI18D, BAI19D, BAI20D, BAI21D, BAI22D, BAI23D,
 COMMON /PTIP/ BAI1P, BAI2P, BAI3P, BAI4P, BAI5P, BAI6P, BAI7P, BAI8P,
 1 BAI9P, BAI10P, BAI11P, BAI12P, BAI13P, BAI14P, BAI15P, BAI16P,
 COMMON /BAIS/ BAI1S, BAI2S, BAI3S, BAI4S, BAI5S, BAI6S, BAI7S, BAI8S,
 1 BAI9S, BAI10S, BAI11S, BAI12S, BAI13S, BAI14S, BAI15S, BAI16S,
 1 BAI17S, BAI18S, BAI19S, BAI20S, BAI21S, BAI22S, BAI23S, BAI24S,
 1 BAI25S, BAI26S, BAI27S, BAI28S, BAI29S, BAI30S, BAI31S, BAI32S,
 1 BAI33S, BAI34S, BAI35S, BAI36S, BAI37S, BAI38S, BAI39S, BAI40S,
 1 BAI41S, BAI42S, BAI43S, BAI44S, BAI45S, BAI46S, BAI47S, BAI48S,
 1 BAI49S, BAI50S, BAI51S, BAI52S, BAI53S, BAI54S, BAI55S, BAI56S,
 1 BAI57S, BAI58S, BAI59S, BAI60S, BAI61S, BAI62S, BAI63S, BAI64S,
 1 BAI65S, BAI66S, BAI67S, BAI68S, BAI69S, BAI70S, BAI71S, BAI72S,
 1 BAI73S, BAI74S, BAI75S, BAI76S, BAI77S, BAI78S, BAI79S, BAI80S,
 1 BAI81S, BAI82S, BAI83S, BAI84S, BAI85S, BAI86S, BAI87S, BAI88S,
 1 BAI89S, BAI90S, BAI91S, BAI92S, BAI93S, BAI94S, BAI95S, BAI96S,
 1 BAI97S, BAI98S, BAI99S, BAI100S, BAI101S, BAI102S, BAI103S,
 1 BAI104S, BAI105S, BAI106S, BAI107S, BAI108S, BAI109S, BAI110S,
 1 BAI111S, BAI112S, BAI113S, BAI114S, BAI115S, BAI116S, BAI117S,
 1 BAI118S, BAI119S, BAI120S, BAI121S, BAI122S, BAI123S, BAI124S,
 1 BAI125S, BAI126S, BAI127S, BAI128S, BAI129S, BAI130S, BAI131S,
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 1 BAI174S, BAI175S, BAI176S, BAI177S, BAI178S, BAI179S, BAI180S,
 1 BAI181S, BAI182S, BAI183S, BAI184S, BAI185S, BAI186S, BAI187S,
 1 BAI188S, BAI189S, BAI190S, BAI191S, BAI192S, BAI193S, BAI194S,
 1 BAI195S, BAI196S, BAI197S, BAI198S, BAI199S, BAI200S, BAI201S,
 1 BAI202S, BAI203S, BAI204S, BAI205S, BAI206S, BAI207S, BAI208S,
 1 BAI209S, BAI210S, BAI211S, BAI212S, BAI213S, BAI214S, BAI215S,
 1 BAI216S, BAI217S, BAI218S, BAI219S, BAI220S, BAI221S, BAI222S,
 1 BAI223S, BAI224S, BAI225S, BAI226S, BAI227S, BAI228S, BAI229S,
 1 BAI230S, BAI231S, BAI232S, BAI233S, BAI234S, BAI235S, BAI236S,
 1 BAI237S, BAI238S, BAI239S, BAI240S, BAI241S, BAI242S, BAI243S,
 1 BAI244S, BAI245S, BAI246S, BAI247S, BAI248S, BAI249S, BAI250S,
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 1 BAI300S, BAI301S, BAI302S, BAI303S, BAI304S, BAI305S, BAI306S,
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CALL READI (NOCB, 'NOCB'  , 1, 19)
CALL READI (NOSP, 'NOSP'  , 1, 19)
CALL READI (NOL, 'NOL'    , 1, 19)
CALL READI (NOS, 'NOS'    , 1, 19)
CALL READI (NODP, 'NODP'  , 1, 19)
CALL READI (NULT, 'NULT'  , 1, 19)
C
C READ IN THE SMOKELIKE CONFIGURATION.
C
CALL READI (NSMOT, 'NSMOT' , 0, 1500)
CALL NSMOT (NSMOT)
C
C INITIALIZE THE SUBSURFACE DRIFT/DIFFUSION MODEL READ.
C
CALL INITSS (SPRYS, PORIV,
C
C INITIALIZE MODEL MASS VARIABLES.
C
NSMTH = 0.0
NSDIO = 0.0
NSBOT = 0.0
NSCLB = 0.0
NSDNI = 0.0
NSLOS = 0.0
NSMFI = 0.0
NSMUI = 0.0
NSMUS = 0.0
C
C INITIALIZE NUMBER OF PARTICLES
C
NORDB (1) = 0
NORDB = 0
NCLN = 0
NSPIL = 0
NFR = 0
NDEF = 0
NLOS = 0
C
C THE FIRST TIME STEP IS REFERRED AS STEP 0.
C
TIME = 0.0
NSTEP = 0
IF (NSTP.EQ.1) WRITE (1) IDAT
IF (NSTP.EQ.1) WRITE (10) IDAT
IF (NSTP.EQ.1) WRITE (11) IDAT
NSAL = 0
C
C DEFINE THE DENSITIES OF THE OIL COMPONENTS
C
DEW (1) = 0.715
DEW (2) = 0.775
DEW (3) = 0.825
DEW (4) = 0.95
DEW (5) = 0.99
DEW (6) = 1.15
DEW (7) = 1.085
DEW (8) = 1.05
C
C READ IF THIS IS A RESTART
C
C
C
C THIS SECTION IS ONLY USED FOR THE RESTART OPTION. IT
C READS THROUGH ALL OF THE PREVIOUS DATA SETS IN ORDER
C TO REACH THE END OF THEM IT DOES THIS IN ORDER TO
C BE ABLE TO WRITE TO THEM WITHOUT WRITING OVER
C PREVIOUS DATA. THIS SECTION ALSO INITIALIZES ALL OF
C VARIABLES TO THE VALUES THEY HAD WHEN THE PREVIOUS RUN
C WAS TERMINATED. THE PARAMETER IBA IS USED TO CONTROL
C THE READING OF THE ENVIRONMENTAL DATA SETS AND BRING THEM
C UP TO THIS TIME STEP
C
IF (NSTP.EQ.0) GO TO 111
WRITE (1,72)
FORNAT ('1')
WRITE (10,73)
FORNAT (21, ' *** THIS IS A RESTARTED RUN *** ')
C
C READ IN RESTART PARAMETERS
C
READ (NORS) NSPTST, NSPT, NSPT, NSPVT, NSPCT, NSPPT
C
IF (NSTP.EQ.0, NSV DATA SETS ARE USED
C
IF (NSTP.EQ.0) GO TO 708
NSTP = NSPT + 1
NSV = NSPT + 1
C
C DETERMINE THE NUMBER OF DATA SETS WHICH HAVE TO
C TO BE READ IN ORDER TO CONTINUE THE RUN.
C
IF (NSPVT.EQ.0) NSPVT = NSPT/NSPVT
IF (NSPCT.EQ.0) NSPCT = NSPT/NSPCT
IF (NSPPT.EQ.0) NSPPT = NSPT/NSPPT
IF (NSPTST.EQ.0) NSPTST = NSPT/NSPTST
IF (NSPCT.EQ.0) NSPCT = NSPT/NSPCT
WRITE (10,324) NSPVT, NSPCT, NSPPT, NSPTST, NSPT
FORNAT (21, ' READ: 1A, VELOCITY 1A, CONCENTRATION 1A,
1 1A, PARTICLE 1A, SPILLER 1A, MASS DATA SETS FOR
2 1A, STEPS')
IF (NSPT.GT.0) READ (NOSP) IDAT11
IF (NSPT.GT.0) READ (NOSP) IDAT1
IF (NSPCT.GT.0) READ (NOCB) IDAT10
C
C READ IN SPILL PARAMETERS
C
IF (NSPT.EQ.0) GO TO 951
DO 700 K=1, NSPT
READ (NOSP,END=901) TIME, NSPIL
WRITE (10,774) TIME, NSPIL
FORNAT (21, F13.5, F13.18, 'SPILLERS')
DO 101 I=1, NSPIL
IF (I.GT.1) READ (NOSP) TIME, NSPIL
READ (NOSP,END=901) I1, NSPIL (1), NSPIL (2), NSPIL (3), NSPIL (4),
1 NSPIL (5), NSPIL (6), NSPIL (7), NSPIL (8), NSPIL (9), NSPIL (10),
101 CONTINUE
700 CONTINUE
GO TO 951
C
C HERE IF AN EOF WAS ENCOUNTERED ON UNIT 1
C
901 CONTINUE

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WRITE (10,801)
FORNAT ('0',50(' '), ' EOF ENCOUNTERED ON UNIT 1')
951 CONTINUE
C
C READ IN CONCENTRATION PARAMETERS
C
IF (NSPCT.EQ.0) GO TO 960
DO 701 J=1, NSPCT
READ (NOCB,END=910) ISUB, JSUB, KSUB, NSUB, NSAL, NSCLASS, NSFLC, NSCP,
1 NSLOS, NSDP, NSIB, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC,
WRITE (10,775) TIME
775 FORNAT (21, ' CONCENTRATION AT TIME ', F20.3, ' READ IN')
READ (NOCB,END=910) (I1(I), I=1, NSUB)
READ (NOCB,END=910) (NSJ(J), J=1, JSUB)
DO 99 K=1, KSUB
99 READ (NOCB,END=910) ((C(1,J,K), I=1, ISUB), J=1, JSUB)
701 CONTINUE
GO TO 960
C
C HERE IF AN EOF WAS ENCOUNTERED ON UNIT 10.
C
910 CONTINUE
WRITE (10,810)
810 FORNAT ('0',50(' '), ' EOF ENCOUNTERED ON UNIT 10')
960 CONTINUE
C
C READ IN PARTICLE PARAMETERS
C
IF (NSPPT.EQ.0) GO TO 961
NSPPT = NSPPT
DO 702 K=1, NSPPT
READ (NOSP,END=911) ISUB, JSUB, KSUB, NSUB, NSAL, NSCLASS, NSFLC, NSCP,
1 NSLOS, NSDP, NSIB, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC,
WRITE (10,774) TIME
774 FORNAT (21, ' PARTICLE POSITIONS AT TIME ', F20.3, ' READ IN')
READ (NOSP,END=911) (I1(I), I=1, ISUB),
READ (NOSP,END=911) (NSJ(J), J=1, JSUB)
DO 450 I=1, NSUB
READ (NOSP,END=911) R, NSRDB (I), NSDIB (I), NSDZB (I), NSDASB (I),
1 DVEL (I), (DCORP (I, JJ), JJ=1, 8)
450 CONTINUE
C
C READ IN PARTICLE POSITIONS
C
DO 66 K=1, NSAL
READ (NOSP,END=911) NSORDB (K), X (K), Y (K), Z (K), ZT
66 CONTINUE
702 CONTINUE
GO TO 961
C
C HERE IF AN EOF WAS ENCOUNTERED ON UNIT 11.
C
911 CONTINUE
WRITE (10)
811 FORNAT ('0',50(' '), ' EOF ENCOUNTERED ON UNIT 11')
961 CONTINUE
C
C READ THROUGH THE MASS DATA SET
C
IF (NSPTST.EQ.0) GO TO 708
DO 703 K=1, NSPTST
READ (NORS,END=912) TBT, ISBAT, ISBIO, ISBOT, ISCLB, ISDNI,
1 ISLOS, ISMFI, ISMUI, ISMUS
WRITE (10,773) TIME
773 FORNAT (21, ' MASS AT TIME ', F20.3, ' READ IN')
703 CONTINUE
GO TO 708
C
C HERE IF AN EOF OF FILE FORNAT ON UNIT 15
C
912 CONTINUE
WRITE (10,812)
812 FORNAT ('0',50(' '), ' EOF ENCOUNTERED ON UNIT 15')
708 IF (NSTP.EQ.-1) NSTP = 0
C
C THIS SECTION READS THE RESTART DATA SET ON UNIT 3
C
C
C READ IN THE VALUES OF THE FOLLOWING VARIABLES WHICH
C WERE PRESENT AT THE TERMINATION OF THE LAST RUN THESE
C ARE WRITTEN OUT AT CERTAIN STEPS AS DETERMINED BY NSMOT
C IN THE SUBROUTINE NSMOT
C
READ (NORS) ISMOT, JSUB, KSUB, NSPVT,
1 NSPCT, NSPPT, NSIB, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC, NSIC,
TIME = TIME + DT
READ (NORS) NSMTH, NSDIO, NSBOT, NSCLB, NSDNI, NSLOS,
1 NSMFI, NSMUI, NSMUS
READ (NORS) NSPIL, NSPIL
DO 55 K=1, NSPIL
READ (NORS) NSPIL (K), NSPIL (K), NSPIL (K),
1 NSPIL (K), NSPIL (K), NSPIL (K), NSPIL (K), NSPIL (K),
2 NSPIL (K), NSPIL (K), NSPIL (K), NSPIL (K), NSPIL (K),
3 NSPIL (K), NSPIL (K), NSPIL (K)
55 CONTINUE
C
C REINITIALIZE NSPIL
C
NSPIL = 0
C
C SKIP PART OF THIS IF THIS IS A PREVIEW RUN
C
IF (NORS.EQ.1) GO TO 332
READ (NORS) NSCLASS
DO 789 I=1, NSCLASS
READ (NORS) NSORDB (I), NSDIB (I), NSDZB (I), NSDASB (I),
1 DVEL (I), (DCORP (I, JJ), JJ=1, 8)
789 CONTINUE
READ (NORS) NSPTST, NSDNI, NSIB, NSIB, NSIB, NSIB, NSIB, NSIB, NSIB,
1 NSIB, NSIB, NSIB
DO 805 I=1, NSAL
READ (NORS) X (I), Y (I), Z (I), NSORDB (I)
805 CONTINUE
332 CONTINUE
READ (NORS) NSCER
IF (NORS.EQ.0) GO TO 65
DO 340 I=1, NSCER
READ (NORS) NSCER (I), NSCER (I), NSCER (I), NSCER (I), NSCER (I),
1 NSCER (I), NSCER (I), NSCER (I), NSCER (I), NSCER (I)
340 CONTINUE

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Figure VII.-3. MAIN

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      NCHFR = 0
05  READ (NCHFR) NCLF
      IF (NCLF.EQ.0) GO TO 111
      DO 501 I = 1, NCLF
        READ (NCHFR) NCLF(I), DCLF(I), ECLF(I), NCLF(I), VCLF(I),
1      ECLF(I), TCLF(I)
501  CONTINUE
      NCLF = 0
C
      FINISH THE RESTART SECTION HERE.
C
111  CONTINUE
C
      READ IN THE DEPTH GRID.
      NOTE: BECAUSE THE FLOATING GRID IS REPRESENTED BY THE DEPTH GRID
      THE DEPTH GRID SHOULD NEVER BE CHANGED IN THE MIDDLE OF A
      RUN, I.E., DO NOT MOVE THIS CALL.
      CALL ABATIN( BDD, BDD, 1, 'BATHYMETRY', DEPTH, DEPTH,
1      BARDI, BARDI, AD, EOL, TOL, EOS, TOS, BDC, BDT)
C
      READ IN THE COMPUTATIONAL CELL GRID
      CALL ABATIN( BCD, BCD, 1, 'COMP CELL', CONF1, COBFP,
1      BAC1, BACT1, AC, ECL, YCL, ECS, TCS, BCONF, BCONF)
      D E C I M I T E R A T I O N H E R E
C
1  CONTINUE
      THIS CONTROL PARAMETER CHECK IS FOR RESTARTING ONLY
      IPI = IPI + 1
      SPAT1 = SPAT1
      IF ((NSTAT.EQ.1).AND.(IPI.LE.BSTEP)) SPAT1 = -1
      IF ((NSTAT.EQ.1).AND.(IPI.GT.BSTEP)) SPAT1 = SPAT1
C
      INCREASE WIND STEP AS SPILL SPREADS AND DISPERSES
C
      READ IN THE STEP CONTROL PARAMETERS AND PRINT OUT VARIABLES READ IN.
      READ (NSTAT) SP, SV, ST, SE, SS, LSPIL, LCLN, LCRN
      FORNAT (55)
      SPAGE = SP * SV * SE * SS * ST
      PAIR = TIME / 3600.0
      NPRINT = ANOD( FLOAT(BSTEP), FLOAT(BSTEP))
      IF ((BSTEP.EQ.1).AND.(IPI.LE.BSTEP)) GO TO 10
      IF (NPRINT.EQ.0) GO TO 247
      WRITE (NSTAT) NPRINT
240  FORNAT ('1', I20(' '), /727, 'SPILL CONTROL PARAMETERS', P8 3,
1  ' BOOTS AFTER THE BEGINNING OF THE SPILL', /' ', I27, '2(' ', ' ') //
2  ' ENVIRONMENTAL DATA READ THIS STEP:')
241  IF (NSTAT.EQ.0) WRITE (NSTAT)
      IF (NSTAT.EQ.0) WRITE (NSTAT)
242  FORNAT (' ', T52, 'CURRENT')
      IF (NSTAT.EQ.0) WRITE (NSTAT)
243  FORNAT (' ', T69, 'TEMPERATURE')
      IF (NSTAT.EQ.0) WRITE (NSTAT)
244  FORNAT (' ', T92, 'SEA STATE')
C
      IF (NSTAT.EQ.0) WRITE (NSTAT)
239  FORNAT (' ', T105, 'TIDAL HEIGHTS')
      IF (NSTAT.EQ.0) WRITE (NSTAT)
245  FORNAT (' ', T60, 'BOOTS')
      WRITE (NSTAT) LSPIL, LCLN, LCRN
246  FORNAT ('0 ADDITION OF SPILLETTS OR SPILL CONTROL EFFORTS',
1  ' THIS STEP', '13', ' SPILLETTS', '15', ' CLEANUP EFFORTS',
2  '15', ' TREATMENT EFFORTS', /' ', I20(' ') //
      SPAGE = SPAGE * SPAT1
247  CONTINUE
      IF (TIME.GT.0.0) GO TO 10
C
      IF THIS IS THE FIRST STEP MAKE SURE THAT ALL REQUIRED DATA
      HAS BEEN READ IN.
      NSTAT = SP * SV * LSPIL * ST
      IF (NSTAT.EQ.0) GO TO 10
      WRITE (NSTAT)
200  FORNAT ('1', 'MISSING INPUT DATA FOR THE FIRST STEP', 'EXIT')
      IF (NSTAT.EQ.0) WRITE (NSTAT)
210  FORNAT ('N', 'N', '13)
      IF (NSTAT.EQ.0) WRITE (NSTAT)
220  FORNAT ('N', 'N', '13)
      IF (LSPIL.EQ.0) WRITE (NSTAT)
230  FORNAT ('N', 'LSPIL', '13)
      IF (NSTAT.EQ.0) WRITE (NSTAT)
231  FORNAT ('N', 'N', '13)
      CALL EXIT
10  CONTINUE
C
      IF WIND VELOCITY FLAG IS SET READ IN NEW WIND ARRAY.
      IF (NSTAT.EQ.1) CALL ABATIN( BWD, BWD, 2, 'WIND VEL', OW, W,
1      BARDI, BARDI, AD, EOL, TOL, EOS, TOS, BWT, BWT)
C
      IF TEMPERATURE FLAG IS SET READ IN NEW TEMPERATURE ARRAY.
      IF (NSTAT.EQ.1) CALL ABATIN( BTD, BTD, 1, 'TEMPERATURE', TTEMP,
1      TTEMP, BARDI, BARDI, AD, EOL, TOL, EOS, TOS, BWT, BWT)
C
      IF SEASTATE FLAG IS SET READ IN NEW SEASTATE ARRAY.
      IF (NSTAT.EQ.1) CALL ABATIN( BSD, BSD, 2, 'SEA STATE', WAVEGT,
1      WAVEGT, BARDI, BARDI, AD, EOL, TOL, EOS, TOS, BWT, BWT)
C
      IF TIDAL VELOCITY FLAG IS SET READ IN NEW TIDAL CURRENT ARRAY.
      IF (NSTAT.EQ.1) GO TO 100
      CALL ABATIN( BTDV, BTDV, 1, 'TIDAL CURRENT', CT, DT, BARDI,
1      BARDI, AT, ETLG, YTLG, YTS, YTS, BWT, BWT)
      CALL ABATIN( BTDV, BTDV, 1, 'TIDAL CURRENT', VT, VT, BARDI,
1      BARDI, AT, ETLG, YTLG, YTS, YTS, BWT, BWT)
100  IF (NSTAT.EQ.1) GO TO 140
      CALL ABATIN( BSL, BSL, 1, 'SIDE LEVEL', BSL, BSL, BARDI,
1      BARDI, AZ, EHL, TEL, RES, TES, BWT, BWT)
110  CONTINUE
C
      IF ONE OR MORE ADDITIONAL CLEANUP EFFORTS THIS STEP READ IN.
      IF (LCLN.EQ.0) .OR. (LSPIL.EQ.1)
1  CALL CLNDR( LCLN, BCLD, SPAGE, NSTAT, IPI, BSTEP)
      IF ONE OR MORE ADDITIONAL TREATMENT EFFORTS THIS STEP READ IN.
      IF (LCRNB.EQ.0) .OR. (NPRINT.EQ.1)
1  CALL CDRNB( LCRNB, BCD, SPAGE, NSTAT, IPI, BSTEP)
      IF ONE OR MORE ADDITIONAL SPILLETTS THIS STEP READ IN.
      IF (LSPIL.EQ.0) .OR. (NPRINT.EQ.1)
1  CALL SPILT( LSPIL, BSPD, SPAGE, NSTAT, IPI, BSTAT,
2  BSPPD, BSPPD)
C
      GO BACK TO THE START IF THIS IS A RESTART AND ALL
      OF THE DATA SETS ARE NOT OF THE CORRECT SIZE.
      IF (NSTAT.EQ.1).AND.(IPI.LE.BSTEP) GO TO 1
      REMOVE OIL BIOLOGICALLY CONSIDERED.
      CALL CORSD
      EVAPORATE, DISSOLVE, DRIFT AND SPREAD OIL SPILLETTS.
      CALL SDPES( I, Y, X, BODDA, BSPAR, BODI, BDD)
      CONVERT PARTICLE POSITION TO TRANSFORMED SYSTEM IF NECESSARY.
      IF (NSTAT.EQ.1).AND.(BODI.GT.0)
1  CALL CVT2( I, Y, X, BPLT, DPLT, BODDA)
      MOVE SUSPENDED OIL DROPLETS
      CALL SODS( I, Y, X, BODDA, C, B, BSTEP, BPLT, DPLT)
      MOVE OIL DEPOSITED ON THE SEA FLOOR.
      CALL BODDPT
      ADD RESURFACED OIL TO EXISTING SPILLETTS OR CREATE NEW SPILLETTS.
      CALL RESPFS
      CALL ADD(COBB)
      LOCATE ALL THE MASS
      CALL MASS( C, M, Y, X, BODDA, BSTEP, BPRINT)
      CONVERT PARTICLE POSITION FROM TRANSFORMED SYSTEM IF NECESSARY.
      IF (NSTAT.EQ.1).AND.(BODI.GT.0)
1  CALL CVT2( -1, I, Y, X, BPLT, DPLT, BODDA)
C
      IF STEP IS MULTIPLE OF BSOBB WRITE OUT TO RESTART DATA SET
      NCH = ANOD(FLOAT(BSTEP), FLOAT(BSOBB))
      IF (NCH.EQ.0).AND.(NSTAT.EQ.0)
1  CALL SUBDDP( I, Y, X, BODDA, BSTEP, BPRINT, BSPPD,
2  BSOB)
C
      INCREASE TIME
      TIME = TIME + DT
      BSTEP = BSTEP + 1
C
      IF TIME LIMIT IS EXCEEDED, TERMINATE THE RUN
      IF (TIME.LT.TIMEL) GO TO 1
C
      SUBDDP THE END OF THE RUN
      BSTEP = BSTEP - 1
      TIME = TIME - DT
      CALL SUBDDP( I, Y, X, BODDA, BSTEP, BPRINT, BSPPD, BSOB)
      E N D P R O G R A M
C
      STOP
      END
      SUBROUTINE DIST(I1, Y1, I2, Y2, BO, ANG, D, ESP, ISPI)
C
      THIS SUBROUTINE CALCULATES DISTANCES
      IF BO = 1 IF ASSUMES THAT THE TWO POINTS ARE
      GIVEN IN LONGITUDE AND LATITUDE AND
      IF CALCULATES THE GREAT CIRCLE DISTANCE
      BETWEEN THEM IN DEGREES.
      IF BO = 2 IF CALCULATES THE X AND Y SPACING BETWEEN
      TWO POINTS GIVEN IN LONGITUDE AND LATITUDE.
      IF BO = 5 IF CALCULATES THE DIFFERENCE BETWEEN THE BOBBITS.
      THIS IS USED WHEN FINDING THE DIFFERENCE BETWEEN
      TWO POINTS WHICH HAVE DISPERSIONS IN DEGREES
      NO BO CONVERSION IS NECESSARY.
      IF ANG = 0 THEN NO ROTATION
      IF ANG > 0 THEN ROTATE COUNTER-CLOCKWISE
      IF ANG < 0 THEN ROTATE CLOCKWISE
      PI=3.14159
      D=6371.0
      SCAL = D*1000.0*PI/180.0
      RAD = PI/180.0
      IF (BO.EQ.2) GO TO 100
      IF (BO.EQ.5) GO TO 400
      B1=SI( I1*BAD)*SI( I2*BAD)
      B2=SI( Y1*BAD)*SI( Y2*BAD)
      B3=COS( I1*BAD)*COS( I2*BAD)*COS( I2*BAD)
      B4=SCOS( B1+B2)
      D=B*5*1000.0
100  CONTINUE
      TSP=( I2-I1)*SCAL
      ESP=( I1-I2)*SCAL*COS( I2*BAD)
      IF (ANG.EQ.0.0) RETURN
      GO TO 500
400  CONTINUE
      ESP=I1-I2
      TSP=I2-I1
      IF (ANG.EQ.0.0) RETURN
500  CONTINUE
      ESP=ESP*COS( ANG)*TSP*SI( ANG)

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TSP=180-ASIN(ARC)*TSP/COS(ARC)
RETURN
END
SUBROUTINE BASIC (C, R, X, Y, Z, HOBDA, BPT, SPRTS)
      SUBROUTINE DESCRIPTION
      IN THIS SUBROUTINE THE MASS OF THOSE PARTICLES LOST
      THROUGH AN OPEN BOUNDARY OR DEPOSITED IS CALCULATED ALONG
      WITH THE REMAINING MASS.
.....
      COMMON STATEMENTS
      COMMON /DEPOS/ BLOST, BDEP
      COMMON /CBTL/ IBSUD, JBSUD, KBSUD, SPRTA,
      SPRTC, DT, TIME, TIRBAI, ISCAL, ISAV(99)
      COMMON /BASS/ IBATH, IBIO, IBOT, IBCLB, IBDBF, IBLCB,
      IBSD, IBSDU, IBSDS
      COMMON /OBT/ OBSP, OBAS, OBCH, OBPT, OBBS, OBTL,
      OBDF, OBUL
      COMMON /PTT/ BCLASS, BUBBD(200), BDIAB(200), BDEB2(200),
      BDESS(200), BVEL2(200), BCOB(200, 8), BTCLAS, BDCSL
      COMMON /SUBS/ STARS, SSOR, BRITS, BRAT, BRAL, PA, DT, DS,
      IALIC, IOLIC, IOIC
.....
      DIMENSION STATEMENTS
      DIMENSION C(15,15,10)
      DIMENSION I(BRAT), J(BRAT), K(BRAT)
      INTEGER N(15,15,10)
      INTEGER*2 BOLDR(BRAT)
.....
      DATA B1 / 6 /
      S T A Y B E E E
.....
      PRINTOUT MASS BALANCE THIS STEP ONLY ONCE PER DAY.
      BPRIT = BBDI / FLOAT(BST), FLOAT(SPRTS)
      IF (SPRTC.EQ.0) BPT=0
      BRITL (BORS) TIME, IBATH, IBIO, IBOT, IBCLB, IBDBF, IBLOS,
      IBSDR, IBSDU, IBSDS
.....
      WRITE (B1,50)
      FORMAT (' ', 120(' '), // 750, 'MASS BALANCE', //, 750, 12(' '))
.....
      PRINT OUT TOTAL AMOUNT OF MASS
      WRITE (B1,5) IBDBP
      FORMAT (' ', 251, 'TOTAL MASS OF OIL SPILLED', 51, F13.5,
      1 21, 'NETRIC TONS', //)
      WRITE (B1,21)
      FORMAT (' ', 71, 'LOCATION OF OIL', 71, 'AMOUNT (NETRIC TONS)',
      1 141, 'PERCENT OF TOTAL')
.....
      PRINT OUT TOTAL AMOUNT IN ATMOSPHERE
      PBT = 100.0 * BRAT / IBDBP
.....
      WRITE (B1,80) IBATH, PBT
      FORMAT (101, 'IN ATMOSPHERE', 74, F13.5, T110, P6.2)
.....
      PRINT OUT TOTAL AMOUNT ON SURFACE
      PBT = 100.0 * IBSDR / IBDBP
      WRITE (B1,55) IBSDU, PBT
      FORMAT (101, 'ON SURFACE', 74, F13.5, T110, P6.2)
.....
      PRINT OUT REMAINING MASS IN WATER COLUMN
      PBT=100.0 * IBSDS/IBDBP
      WRITE (B1,20) BRAT, IBSDS, PBT
      FORMAT (101, 'IN WATER COLUMN', 73, 15, 'BARREL PARTICLES', 74,
      1 713.5, T110, P6.2)
.....
      PRINT OUT AMOUNT ON BOTTOM
      PBT = 100.0 * IBBOT/IBDBP
      WRITE (B1,60) IBOT, IBBOT, PBT
      FORMAT (101, 'ON BOTTOM', 73, 15, 'DEPOSITED PARTICLES', 74,
      1 713.5, T110, P6.2)
.....
      PRINT OUT AMOUNT OF THE SHORE
      PBT= 100.0 * IBKSR/IBDBP
      WRITE (B1,62) IBKSL, PBT
      FORMAT (101, 'OF SHORE', 74, F13.5, T110, P6.2)
      WRITE (B1,63)
      FORMAT (71, 'REMOVAL RECAUSERS')
.....
      PRINT OUT AMOUNT BIOLOGICALLY CONSUMED
      PBT = 100.0 * IBIO/IBDBP
      WRITE (B1,70) IBIO, PBT
      FORMAT (101, 'BIOLOGICALLY CONSUMED', 74, F13.5, T110, P6.2)
.....
      PRINT OUT AMOUNT PHYSICALLY CLEARED UP
      PBT = 100.0 * IBCLB/IBDBP
      WRITE (B1,64) IBCLB, PBT
      FORMAT (101, 'PHYSICALLY CLEARED UP', 74, F13.5, T110, P6.2)
.....
      AMOUNT LOST THROUGH BOUNDARIES
      PBT = 100.0 * IBLOS/IBDBP
      WRITE (B1,60) BLOST, IBLOS, PBT
      FORMAT (101, 'LOST THROUGH OPEN BOUNDARY', 73, 15, 'LOST PARTICLES',
      1 774, F13.5, T110, P6.2/2(' ', 120(' ')/))
      S T O P S S E E
.....
      RETURN
      END
      SUBROUTINE ROTAT(EL, VL, ED, VD, ARC, EO, VO, EC, VC)
      THIS SUBROUTINE CONVERTS THE POSITIONS EO, VO, WHICH ARE
      GIVE RESPECT TO THE DEPTH GRID
      TO POSITIONS EL, VL RESPECT TO A SURF GRID
      AS DEFINED BY EL, VL, ED, VD, ARC.
      WHERE EL AND VL ARE THE LONGITUDE AND LATITUDE

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```

      OF THE SURF GRID. ED AND VD ARE THE GRID SEPARATIONS.
      ARC AND EL IS THE ANGLE WITH RESPECT TO LINES OF CONSTANT
      LATITUDE.
.....
      COMMON /SUBS/ STARS, SSOR, BRITS, BRAT, BRAL, PA, DT, DS,
      IALIC, IOLIC, IOIC
      COMMON /CBTL/ IBSUD, JBSUD, KBSUD, SPRTA,
      SPRTC, DT, TIME, TIRBAI, ISCAL, ISAV(99)
      COMMON /OBT/ OBSP, OBAS, OBCH, OBPT, OBBS, OBTL,
      OBDF, OBUL
      COMMON /PTT/ BCLASS, BUBBD(200), BDIAB(200), BDEB2(200),
      BDESS(200), BVEL2(200), BCOB(200, 8), BTCLAS, BDCSL
      COMMON /SUBS/ STARS, SSOR, BRITS, BRAT, BRAL, PA, DT, DS,
      IALIC, IOLIC, IOIC
.....
      NO = 2
      IP (ISCAL.EQ.2) NO = 5
      ED = ARC - 10
      IS = 100COS(ARC)+100SIN(ARC)
      TS = 100SIN(ARC)+100COS(ARC)
.....
      CALCULATE DISTANCE BETWEEN ORIGINS
      CALL DIST(ED, VL, EL, VL, NO, ARC, D, ESP, TSP)
      ED = IS - ISF
      TD = TS - TSP
      EC = ED/ED + 1.0
      VC = TD/TD + 1.0
      RETURN
      END
.....
      SUBROUTINE ARAT1(ED, ED, NO, SARC, ARAT1, ARAT2, IBAT,
      1 JBAT, ANGLE, EL, VL, ES, VS, BARAT1, BARAT2)
.....
      SUBROUTINE DESCRIPTION
      THIS SUBROUTINE READS IN ONE OR TWO ARRAYS FOR THE VARIOUS
      GRIDS USED IN THE PROGRAM, SPECIFICALLY THE DEPTH GRID, THE
      GRID VELOCITY GRID, THE TEMPERATURE GRID AND THE SURF STATE
      GRID.
.....
      VARIABLE DESCRIPTION
      SUBROUTINE ARGUMENTS
      (1) NO - FORMAT CONTROL: 1 - UNFORATTED READ;
      2 - UNFORATTED INTEGER;
      3 - FORATTED READ;
      4 - FORATTED INTEGER.
      (2) ED - UNIT # DATA IS TO BE READ FROM.
      (3) NO - # OF ARRAYS TO BE READ IN.
      (4) SARC - DESCRIPTOR FOR VARIABLE TO BE READ IN.
      (5) ARAT1 - FIRST ARRAY READ IN.
      (6) ARAT2 - SECOND ARRAY READ IN.
      (7) IBAT - # OF ELEMENTS IN I IN THE INPUT ARRAYS.
      (8) JBAT - # OF ELEMENTS IN J IN THE INPUT ARRAYS.
      (9) ANGLE - ANGLE BETWEEN THE I AXIS FOR THE INPUT VARIABLES
      AND LINES OF CONSTANT LATITUDE.
      (10) EL - LONGITUDE OF THE ORIGIN OF THE FLOATING GRID.
      (11) VL - LATITUDE OF THE ORIGIN OF THE FLOATING GRID.
      (12) ES - GRID SPACING IN I.
      (13) VS - GRID SPACING IN J.
      (14) BARAT1 - EQUIVALENCED TO ARAT1 IN THE CALLING PROGRAM
.....
      (15) BARAT2 - EQUIVALENCED TO ARAT2 IN THE CALLING PROGRAM
.....
      OTHER VARIABLES USED IN THE SUBROUTINE
      BAR - THE DESCRIPTOR OF THE INPUT VARIABLE STORED
      WITH THE DATA.
      VAR1 - 2- BAR1 OF ARAT1 TO BE USED IN PRINTOUT HEADS.
      VAR2 - 2- BAR2 OF ARAT2 TO BE USED IN PRINTOUT HEADS.
      UNIT1 - 3- UNITS OF ARAT1 TO BE USED IN PRINTOUT HEADS.
      UNIT2 - 3- UNITS OF ARAT2 TO BE USED IN PRINTOUT HEADS.
.....
      NOTE 1: THE ARRAYS ARAT1 AND ARAT2 ARE EQUIVALENCED IN THE
      MAIN PROGRAM TO THE ARRAYS BARAT1 AND BARAT2. THE
      PARAMETER NO DETERMINES IF AN INTEGER OR A FLOATING
      POINT VALUE IS TO BE READ IN.
.....
      COMMON STATEMENTS
      COMMON /CBTL/ IBSUD, JBSUD, KBSUD, SPRTA,
      SPRTC, DT, TIME, TIRBAI, ISCAL, ISAV(99)
      COMMON /OBT/ OBSP, OBAS, OBCH, OBPT, OBBS, OBTL,
      OBDF, OBUL
      COMMON /PTT/ BCLASS, BUBBD(200), BDIAB(200), BDEB2(200),
      BDESS(200), BVEL2(200), BCOB(200, 8), BTCLAS, BDCSL
      COMMON /SUBS/ STARS, SSOR, BRITS, BRAT, BRAL, PA, DT, DS,
      IALIC, IOLIC, IOIC
.....
      DIMENSION STATEMENTS
      DIMENSION ARAT1( 30, 30), ARAT2( 30, 30), BAR(3), BAR2(3)
      DIMENSION V1(2), V12(2), UNIT1(3), UNIT2(3)
      DIMENSION ES(15), BARAT1( 30, 30), BARAT2( 30, 30)
      DIMENSION ARAT12( 30, 30)
.....
      DATA STATEMENTS
      DATA PI, EW / 3.14159, 6 /
      DATA E1 / 1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15 /
      DATA BAR1, BAR2 / 'UTID', 'VTID' /
.....
      S T A Y B E E E
.....
      DETERMINE DIMENSIONS OF GRIDS
      READ IN GRID DEFINITION VARIABLES (FORATTED).
      IF (NO.EQ.2) GO TO 20
      READ (NO,100) BAR, VAR1, UNIT1, VAR2, UNIT2
      FORMAT (13A)
      READ (NO,105) IBAT, JBAT, ANGLE, EL, VL, ES, VS, UNIT3
      FORMAT (215,3P10.6,2P10.6,2A)
      GO TO 25
.....
      READ IN GRID DEFINITION VARIABLES (UNFORATTED).
      20 CONTINUE
      READ (NO) BAR, VAR1, UNIT1, VAR2, UNIT2
      READ (NO) IBAT, JBAT, ANGLE, EL, VL, ES, VS, UNIT3
.....
      CHECK THAT THIS IS THE DATA REQUESTED.
      25 CONTINUE
      DO 900 I=1,3

```

Figure VII.-3. MAIN

```

IF (NAB(1),NAB(2)) GO TO 999
900 CONTINUE
C
C TEST IF THE DIMENSIONS ARE RIGHT
C
IF ((ISCAL.EQ.1).AND.(IS.GT.5.0)) GO TO 41
IF ((ISCAL.EQ.1).AND.(IS.LT.5.0)) GO TO 41
IF ((ISCAL.EQ.2).AND.(IS.LT.5.0)) GO TO 41
IF ((ISCAL.EQ.2).AND.(IS.LT.5.0)) GO TO 41
WRITE (99,57) ISCAL,IS,IS
67 FORNAT (50(' '),/21,'DIMENSIONS DO NOT MATCH')
1 ISCAL = '13,61,15 =',P10.3,61,'IS =',P10.3)
STOP
81 CONTINUE
IF (ISCAL.EQ.1) GO TO 42
IF (ISCAL.EQ.2.AND.ANGLE.EQ.0.0) GO TO 42
WRITE (99,63) ANGLE
63 FORNAT (100(' '),/21,'ISCAL = 2 AND ANGLE =',P10.3)
STOP
42 CONTINUE
1 IF (SPRTA) 10,11,12
C
C WRITE GRID DEFINITION VARIABLES AND HEADER IF OUTPUT REQUESTED.
C
12 CONTINUE
PRIT = TIME / 3600.0
WRITE (99,200) BAR, PRIT, BAR, IBAR, ES, OBIT53, JBAR, IS, OBIT53
FORNAT ('1',401,3A4,' INPUT DATA ',P10.2,' BOARDS AFTER',
1 ' THE BEGINNING OF THE SPILL',/41,'THE ',3A4,
2 ' GRID HAS ',15,' DIVISIONS IN X SPACED ',P12.4,
3 ' ',2A4,' SPRT',/41,'SU ',15,
4 ' DIVISIONS IN Y SPACED ',P12.4,12,2A4,' SPRT',/4)
WRITE (99,210) BAR, IL, IL
210 FORNAT (41,'THE (1,1) GRID LOCATION OF THE ',3A4,
1 ' COORDINATE SYSTEM IS AT ',
2 ' P10.4,' DEGREES LONGITUDE AND ',P10.6,
3 ' DEGREES LATITUDE',/4)
IF (ANGLE.NE.0.0) WRITE (99,215) BAR, ANGLE
215 FORNAT (41,'FINALLY THE X AXIS OF THE ',3A4,
1 ' GRID BARES AN ANGLE (COUNTERCLOCKWISE) OF',P10.6,
2 ' DEGREES WITH LINES OF',/41,'CONSTANT LATITUDE',/4)
ANGLE = ANGLE + PI / 100.0
GO TO 10
C
C HERE ONLY IF THE SHORT DIAGNOSTIC FORM IS DESIRED.
C
C
11 CONTINUE
TSI = TIME / 3600.0
WRITE (99,230) BAR, TSI
230 FORNAT (41,'THE ',3A4,' INFORMATION IS BEING READ IN',P10.4,
1 ' BOARDS INTO THE SPILL',/4)
C
C HERE TO READ IN THE DATA.
C
C
10 CONTINUE
C
C BRANCH TO READ DIFFERENT FORNAT TYPES.
C
C
80 GO TO (40,80,60,70), 80
C
C
C HERE TO READ UNFORNATTED REAL VARIABLES
C
80 CONTINUE
READ (99) ((ABRAT1(I,J),I=1,IBAR),J=1,JBAR)
IF (99.EQ.1) GO TO 80
READ (99) ((ABRAT2(I,J),I=1,IBAR),J=1,JBAR)
GO TO 80
C
C HERE TO READ UNFORNATTED INTEGER VARIABLES.
C
C
50 CONTINUE
READ (99) ((ABRAT1(I,J),I=1,IBAR),J=1,JBAR)
IF (99.EQ.1) GO TO 90
READ (99) ((ABRAT2(I,J),I=1,IBAR),J=1,JBAR)
GO TO 90
C
C HERE TO READ FORNATTED REAL VARIABLES.
C
C
60 CONTINUE
DO 62 J=1,JBAR
READ (99,110) (ABRAT1(I,J),I=1,IBAR)
110 FORNAT (1076.2)
62 CONTINUE
IF (99.EQ.1) GO TO 60
DO 64 J=1,JBAR
READ (99,110) (ABRAT2(I,J),I=1,IBAR)
64 CONTINUE
GO TO 60
C
C HERE TO READ FORNATTED INTEGER VARIABLES.
C
C
70 CONTINUE
DO 72 J=1,JBAR
READ (99,120) (ABRAT1(I,J),I=1,IBAR)
120 FORNAT (1514)
72 CONTINUE
IF (99.EQ.1) GO TO 70
DO 74 J=1,JBAR
READ (99,120) (ABRAT2(I,J),I=1,IBAR)
74 CONTINUE
GO TO 70
C
C HERE TO PRINT REAL ARRAYS.
C
C
80 CONTINUE
IF (SPRTA.LE.0) RETURN
DO 96 I = 1,IBAR
DO 96 J = 1,JBAR
ABRAT1(I,J) = ABRAT1(I,J)
ABRAT2(I,J) = ABRAT2(I,J)
96 SPRT = 0
C
C THIS FILLS THE REAL ARRAYS IF ISCAL = 2
C
IF (ISCAL.EQ.1) GO TO 56
IF (BAR(1).EQ.BAR(1)) GO TO 55
IF (BAR(1).NE.BAR(2)) GO TO 56
95 SPRT = 1
WRITE (99,24)
24 FORNAT (12,' ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED',
1 ' BY 10 ** -6')
54 CONTINUE
IBAR1 = IBAR
IF (IBAR1.GT.15) IBAR1 = 15
WRITE (99,220) BAR1, OBIT51, (KI(I),I=1,IBAR1)
220 FORNAT (//501,2A4,' VALUES IN OBITS OF ',3A4//41,'1,551,
1 ' ELEMENTS',/12,'ELEMENTS',31,15(12,41)//1)
IF (SPRT.NE.1) GO TO 77
DO 71 I=1,IBAR1
DO 71 J=1,JBAR1
71 ABRAT1(I,J) = ABRAT1(I,J)*(10**6.0)
77 CONTINUE
J = J - 1
DO 82 I=1,IBAR1
WRITE (99,240) J, (ABRAT1(I,J),I=1,IBAR1)
240 FORNAT ('0',14,5E,15(12,7.3)/(81.15(12,7.3)))
82 CONTINUE
IF (99.EQ.1) RETURN
IF (SPRT.NE.1) GO TO 79
DO 76 I=1,IBAR1
DO 76 J=1,JBAR1
76 ABRAT2(I,J) = ABRAT2(I,J) * (10**6.0)
79 CONTINUE
WRITE (99,220) BAR2, OBIT52, (KI(I),I=1,IBAR1)
J = JBAR1 + 1
DO 84 I=1,IBAR1
WRITE (99,240) J, (ABRAT2(I,J),I=1,IBAR1)
84 CONTINUE
RETURN
C
C HERE TO PRINT INTEGER ARRAYS
C
C
90 CONTINUE
IF (SPRTA.LE.0) RETURN
IBAR1 = IBAR
IF (IBAR1.GT.15) IBAR1 = 15
WRITE (99,220) BAR1, OBIT51, (KI(I),I=1,IBAR1)
J = JBAR1 + 1
DO 92 I=1,IBAR1
WRITE (99,250) J, (ABRAT1(I,J),I=1,IBAR1)
250 FORNAT (12,15,2A,15(12,3A,21))
92 CONTINUE
IF (99.EQ.1) RETURN
WRITE (99,220) BAR2, OBIT52, (KI(I),I=1,IBAR1)
J = JBAR1 + 1
DO 94 I=1,IBAR1
WRITE (99,250) J, (ABRAT2(I,J),I=1,IBAR1)
94 CONTINUE
RETURN
C
C HERE IF THERE IS PROBLEMS WITH THE VARIABLE NAME.
C
C
999 CONTINUE
WRITE (99,260) BAR, BAR
260 FORNAT (101,'FATAL ERROR',/101,3A4,' REQUESTED ',
1 ' 3A4,' READ IN. ACTION TAKEN - SUBROUT AND EXIT.')
```

Figure VII.-3. MAIN

```
230      WRITE (N1,230) I, VCLR(1), VCLR(2), VCLR(3)
      FORMAT('1. THE "1A" CLEARSP EFFORT CORRECTLY UNDERWAY',
      ' IS CENTERED AT LONGITUDE ',F10.6,' AND LATITUDE ',
      F10.6/49,' THE RADIIUS OF COVERAGE OF THIS EFFORT IS ',
      F10.1, ' METERS')
      WRITE (N1,240) VCLR(2), VCLR(3)
      FORMAT('1. THE RADIIUS OF RECOVERY IS ',F10.6,'
      ' METERS/SECOND WITH AN EFFICIENCY OF ',F10.4,'%')
240      WRITE (N1,250) VCLR(1), VCLR(2)
      FORMAT('1. THIS CLEARSP STARTS ',F10.6,' HOURS AFTER THE
      ' BEGINNING OF THE SPILL AND LASTS ',F10.6,' HOURS')
10      CONTINUE
      UPDATE THE CLEARSP COORDS.
      VCLR = JCLR
      RETURN
28      CONTINUE
      IF (NCLR.EQ.0) RETURN
      READ (ID,100) VCLR, DC1, VCL, VCL, VCL, VCL, VCL
      WRITE (N1,31) I, J
      FORMAT('1. AT STEP ',I,' OLD CLEARSP INFORMATION READ IS')
      VCLR = JCLR
      WBT = (VCLR-DC1)*3600.0
      IF (TIME.GT.WBT) VCLR=VCLR-1
      END STATEMENT
      RETURN
      SUBROUTINE CHECKS (LCRCH, ED, SPACE, BSTEP, ISE, BSTEP)
      THIS SUBROUTINE READS IN THE CHEMICAL TREATMENT EFFORT
      PROPERTIES AND PRINTS THEM OUT.
      CORCOR STATEMENTS
      CORCOR /CWER/ VCHR(1), VCHR(10), DCWER(10), ACWER(10),
      1 VCHR(10), VCHR(10), VCHR(10), VCHR(10), VCHR(10),
      2 VCHR(10), VCHR(10)
      CORCOR /CWT/ JCSR, JCSR, JCSR, BSR, BSR,
      1 BSR, DT, TIME, TIBAR, ISCAL, BSR(99)
      DATA STATEMENTS
      DATA N1/4
      START STATEMENT
      WRITE OUT HEADS AND TIME FOR THIS STEP.
      JCSR = ACWER + LCWER
      IF (JCSR.LE.0) RETURN
      GO TO ANOTHER SECTION IF THIS IS A RESTART
      IF (BSTEP.EQ.1).AND.(ISE.LE.BSTEP) GO TO 20
      IF (PAGE.GE.1) WRITE (N1,201)
201      PRINT = TIME / 3600.0
      WRITE (N1,200) PRINT
200      FORMAT('0. T15, CHEMICAL TREATMENT EFFORTS IN PROGRESS',
      1 F10.6, ' HOURS AFTER THE BEGINNING OF THE SPILL',
      2 ' ',F15.8,' ')
      DO LOOP OVER ALL CURRENT TREATMENT EFFORTS.
      IF (VCHR.GT.0) WRITE (N1,210)
210      FORMAT('01. CONTINUING TREATMENT EFFORTS THIS STEP')
      GO TO 1+JCSR
      IF (JCSR-1) 20, 21, 22
21      CONTINUE
      WRITE (N1,220)
220      FORMAT('02. NEW TREATMENT EFFORTS BEGIN THIS STEP')
22      CONTINUE
      READ (N1,100) VCHR(1), DCWER(1), VCHR(1), VCHR(1), VCHR(1),
      1 VCHR(1), VCHR(1), VCHR(1), VCHR(1), VCHR(1)
      100      FORMAT('03. TREATMENT EFFORTS')
      CONTINUE
      PRINT OUT ALL TREATMENT DATA FOR CURRENT EFFORTS.
      TERE = VCHR(1) / VCHR(1)
      WRITE (N1,230) I, VCHR(1), VCHR(1), VCHR(1), TERE, VCHR(1)
      FORMAT('1. THE "1A" CHEMICAL TREATMENT EFFORTS',
      1 ' IS CENTERED AT LONGITUDE ',F10.6,' AND LATITUDE ',
      2 F10.6/49,' THE RADIIUS OF COVERAGE OF THIS SPILL',
      3 ' IS ',F10.1,' METERS',
      4 ' WITH AN EFFICIENCY OF ',F10.4,'%')
      WRITE (N1,240) VCHR(1)
      FORMAT('1. THE RADIIUS OF RECOVERY IS ',F10.6,' METERS',
      1 ' WITH AN EFFICIENCY OF ',F10.4,'%')
      WRITE (N1,250) VCHR(1), DCWER(1)
      FORMAT('1. THIS TREATMENT EFFORT STARTS ',F10.6,' HOURS',
      1 ' AFTER THE BEGINNING OF THE SPILL AND LASTS ',F10.6,'
      2 ' HOURS.')
      WRITE (N1,260) VCHR(1)
      FORMAT('1. THIS TREATMENT EFFORT LOWERS THE INTERFACIAL',
      1 ' TENSION TO ',F10.6/49)
      CONTINUE
      STORE THE BOUNDS OF CURRENT TREATMENT EFFORTS.
      VCSR = JCSR
      RETURN
28      CONTINUE
      IF (LCRCH.EQ.0) RETURN
      READ (N1,100) VCHR, DCW, VCHR, VCHR, VCHR,
      1 VCHR, VCHR, VCHR, VCHR, VCHR,
      2 VCHR, VCHR, VCHR, VCHR, VCHR,
      31      FORMAT('1. AT STEP ',I,' OLD TREATMENT INFO READ IS')
      VCSR = JCSR
      WBT = (VCSR-DCW)*3600.0
      IF (TIME.GT.WBT) VCSR=VCSR-1
      END STATEMENT
      RETURN
      SUBROUTINE CHECKS (LCRCH, ED, SPACE, BSTEP, ISE, BSTEP)
      THIS SUBROUTINE READS IN THE CHEMICAL TREATMENT EFFORT
      PROPERTIES AND PRINTS THEM OUT.
      CORCOR STATEMENTS
      CORCOR /CWER/ VCHR(1), VCHR(10), DCWER(10), ACWER(10),
      1 VCHR(10), VCHR(10), VCHR(10), VCHR(10), VCHR(10),
      2 VCHR(10), VCHR(10)
      CORCOR /CWT/ JCSR, JCSR, JCSR, BSR, BSR,
      1 BSR, DT, TIME, TIBAR, ISCAL, BSR(99)
      DATA STATEMENTS
      DATA N1/4
      START STATEMENT
      WRITE OUT HEADS AND TIME FOR THIS STEP.
      JCSR = ACWER + LCWER
      IF (JCSR.LE.0) RETURN
      GO TO ANOTHER SECTION IF THIS IS A RESTART
      IF (BSTEP.EQ.1).AND.(ISE.LE.BSTEP) GO TO 20
      IF (PAGE.GE.1) WRITE (N1,201)
201      PRINT = TIME / 3600.0
      WRITE (N1,200) PRINT
200      FORMAT('0. T15, CHEMICAL TREATMENT EFFORTS IN PROGRESS',
      1 F10.6, ' HOURS AFTER THE BEGINNING OF THE SPILL',
      2 ' ',F15.8,' ')
      DO LOOP OVER ALL CURRENT TREATMENT EFFORTS.
      IF (VCHR.GT.0) WRITE (N1,210)
210      FORMAT('01. CONTINUING TREATMENT EFFORTS THIS STEP')
      GO TO 1+JCSR
      IF (JCSR-1) 20, 21, 22
21      CONTINUE
      WRITE (N1,220)
220      FORMAT('02. NEW TREATMENT EFFORTS BEGIN THIS STEP')
22      CONTINUE
      READ (N1,100) VCHR(1), DCWER(1), VCHR(1), VCHR(1), VCHR(1),
      1 VCHR(1), VCHR(1), VCHR(1), VCHR(1), VCHR(1)
      100      FORMAT('03. TREATMENT EFFORTS')
      CONTINUE
      PRINT OUT ALL TREATMENT DATA FOR CURRENT EFFORTS.
      TERE = VCHR(1) / VCHR(1)
      WRITE (N1,230) I, VCHR(1), VCHR(1), VCHR(1), TERE, VCHR(1)
      FORMAT('1. THE "1A" CHEMICAL TREATMENT EFFORTS',
      1 ' IS CENTERED AT LONGITUDE ',F10.6,' AND LATITUDE ',
      2 F10.6/49,' THE RADIIUS OF COVERAGE OF THIS SPILL',
      3 ' IS ',F10.1,' METERS',
      4 ' WITH AN EFFICIENCY OF ',F10.4,'%')
      WRITE (N1,240) VCHR(1)
      FORMAT('1. THE RADIIUS OF RECOVERY IS ',F10.6,' METERS',
      1 ' WITH AN EFFICIENCY OF ',F10.4,'%')
      WRITE (N1,250) VCHR(1), DCWER(1)
      FORMAT('1. THIS TREATMENT EFFORT STARTS ',F10.6,' HOURS',
      1 ' AFTER THE BEGINNING OF THE SPILL AND LASTS ',F10.6,'
      2 ' HOURS.')
      WRITE (N1,260) VCHR(1)
      FORMAT('1. THIS TREATMENT EFFORT LOWERS THE INTERFACIAL',
      1 ' TENSION TO ',F10.6/49)
      CONTINUE
      STORE THE BOUNDS OF CURRENT TREATMENT EFFORTS.
      VCSR = JCSR
      RETURN
28      CONTINUE
      IF (LCRCH.EQ.0) RETURN
      READ (N1,100) VCHR, DCW, VCHR, VCHR, VCHR,
      1 VCHR, VCHR, VCHR, VCHR, VCHR,
      2 VCHR, VCHR, VCHR, VCHR, VCHR,
      31      FORMAT('1. AT STEP ',I,' OLD TREATMENT INFO READ IS')
      VCSR = JCSR
      WBT = (VCSR-DCW)*3600.0
      IF (TIME.GT.WBT) VCSR=VCSR-1
      END STATEMENT
      RETURN
```

Figure VII.-3. MAIN


```

STOP
100 WRITE (80,30) I, ISHAI
30 FORNAT (21,F10.5,5A1,A8)
RETURN
END
SUBROUTINE SHOR2(BD)
C
C THIS SUBROUTINE READS IN THE LONGITUDE AND LATITUDE OF
C SHORELINE POINTS.
C
C .....
C COMMON STATEMENTS
COMMON /SHOR/ BSHOR, LSHOR(1500), TSHOR(1500)
C
C DATA STATEMENTS
DATA 80 / 6 /
START HERE
C
IF (BSHOR.EQ.0) RETURN
WRITE (80,75) BSHOR
75 FORNAT (21,/, ' THERE ARE ',I4,' SHORELINE POINTS')
C
READ (80) ISHOR
READ (80) TSHOR
C
END HERE
C
RETURN
END
SUBROUTINE SPILL2(LSPIL, BD, SPAGE, BSTEP, IES, BSTEP,
1 BPPED, BPPED)
C
C THIS SUBROUTINE READS IN ALL NEW SPILLET'S THIS STEP AND
C PRINTS OUT THE APPROPRIATE DATA OF ALL CURRENT SPILLET'S.
C SOME VARIABLES
BPPED = INTERVAL PRINT CONTROL FOR OUTPUT TO PAPER
BPPED = INTERVAL PRINT CONTROL FOR OUTPUT TO DISK
C
C .....
C COMMON STATEMENTS
COMMON /CSTL/ ISHOB, JSHOB, KSHOB, SPETA,
1 SPATC, DT, TIBI, TIRAB, ISCAL, USAV(99)
COMMON /BASS/ IBATB, IBIBO, IBBOT, IBCLB, IBDBP, IBLOS,
1 IBSHI, IBSHU, IBSSU
COMMON /ODTF/ BOSH, BUSH, BUCB, BDPY, BORS, BULT,
1 BDDP, BUVL
COMMON /SPIL/ BSPIL, BSPIL, ASPIL(99), BSPIL(99), DSPIL(99),
1 PSPIL(99), CSPIL(99,8), BSPIL(99), SSPIL(99),
2 TSPIL(99), YSPIL(99), OSPIL(99), BSPIL(99),
3 TSPIL(99), SSPIL(99), BAISSL
DIMENSION CSPT(10)
C
C DATA STATEMENTS
DATA 80/6/
C
START HERE
C
PRINT OUT HEADER AND TIME OF THIS STEP.
BPRINT=0
BPII = 0
JSPIL = BSPIL + LSPIL
FOR RESTARTING, SKIP TO END OF THE SUBROUTINE
IF (BSTEP.EQ.1).AND.(IIE.LE.BSTEP) GO TO 28
DETERMINE THE PRINT CONTROL PARAMETERS FOR THIS STEP
IF (BPPED.LT.0) GO TO 79
IF (BPPED.EQ.0).AND.(TIME.EQ.0.0) BPII = 1
IF (BPPED.LT.0) GO TO 79
BSTEP = ABS(FLOAT(BSTEP),FLOAT(BPPED))
IF (BSTEP.EQ.0) BPII=1
79 CONTINUE
IF (BPPED.LT.0) GO TO 80
IF (BPPED.EQ.0).AND.(TIME.EQ.0.0) BPRINT=1
IF (BPPED.LT.0) GO TO 80
BSTEP = ABS(FLOAT(BSTEP),FLOAT(BPPED))
IF (BSTEP.EQ.0) BPRINT = 1
80 CONTINUE
BPII = TIME/3600.0
IF (BPII.LT.0) GO TO 85
IF (JSPIL.LT.0) RETURN
IF (SPAGE.GE.1) WRITE (80,201)
FORNAT (' ')
WRITE (80,200) BPII
200 FORNAT ('0',I29,' EXISTING SPILLET'S ',F8.3,' HOURS AFTER',
1 ' THE BEGINNING OF THE SPILL',/,I29,'(1-1)')
C
DO LOOP OVER ALL EXISTING SPILLET'S.
IF (BSPIL.GT.0) WRITE (80,210)
210 FORNAT (301,' SPILLET'S CREATED PRIOR TO THIS STEP')/
CONTINUE
IF (JSPIL.LE.0) RETURN
DO 10 I=1,JSPIL
21 CONTINUE
IF (BPII.EQ.0) GO TO 22
WRITE (80,220)
220 FORNAT ('0',I29,' NEW SPILLET'S ADDED THIS STEP')/
CONTINUE
READ (80,100) BSPIL(I),DSPIL(I),ASPIL(I),SSPIL(I),TSPIL(I),
100 BSPIL(I),SPIL(I),BSPIL(I),TSPIL(I)
FORNAT (80,3,80,2,2F8,3)
READ (80,101) (CSPIL(I,J),J=1,BSPIL)
FORNAT (805,2)
101
BSPIL(I) IS SET EQUAL TO TIME HERE. THIS IS FOR SUBSEQUENT.
BSPIL(I) = TIME
AND PASS TO EXISTING PASS

```

```

1000 BSHOR = BSHOR + BSPIL(I)
1001 BSHOR = BSHOR + BSPIL(I)
CONTINUE
C
PRINT OUT ALL SPILLET PARAMETERS.
C
BPII = BSPIL(I) / 3600.0
IF (BPII.EQ.0) GO TO 23
WRITE (80,230) I, BPII, TSPIL(I), YSPIL(I), BSPIL(I),
1 BSPIL(I)
230 FORNAT (41,' THE ',I29,' SPILLET APPEARED ',F8.2,
1 ' HOURS AFTER THE BEGINNING OF THE SPILL',/,I1,15,
2 ' CENTERED AT LONGITUDE ',F10.6,' AND LATITUDE ',F10.6,
3 ' ,',/,I4,' IS OF RADIUS ',F10.2,
4 ' METERS AND IS OF WEIGHT ',F10.6,' METRIC TONS. ')
WRITE (80,240) DSPIL(I), BSPIL(I), BSPIL(I)
240 FORNAT (41,' SOME PROPERTIES OF THE SPILLED OIL ARE: '/
1 ' 201,' DENSITY ',F10.6,' G/CM3',/,
2 ' INTERFACIAL TENSION ',F10.6,' DYNES/CM',/,
3 ' KINEMATIC VISCOSITY ',F10.6,' CENTISTOKES')
WRITE (80,250) (CSPIL(I,J),J=1,BSPIL)
250 FORNAT (41,' BY WEIGHT THE OIL FRACTIONS ARE: ',I29,
1 ' PARAFFIN (C6-C12)',/,F10.6/501,
2 ' PARAFFIN (C13-C22)',/,F10.6/501,
3 ' CYCLOPARAFFIN (C6-C12)',/,F10.6/501,
4 ' CYCLOPARAFFIN (C13-C22)',/,F10.6/501,
5 ' AROMATIC (C6-C11)',/,F10.6/501, ' AROMATIC (C12-C16)',
6 ' ,',/,F10.6/501, ' NAPHTHENO-AROMATIC (C9-C25)',
7 ' ,',/,F10.6/501, ' RESIDUAL',/,F10.6)
23 CONTINUE
C
WRITE SPILLET DEFINITIONS OUT TO DISK
C
IF (BPII2.EQ.0) GO TO 24
WRITE (1) TIME,JSPIL
WRITE (1) I,BPII,TSPIL(I),YSPIL(I),BSPIL(I),BSPIL(I),
1 DSPIL(I),SSPIL(I),OSPIL(I),CSPIL(2,J),J=1,8)
CONTINUE
24
INITIALIZE FRACTION OF SPILL TREATED VARIABLE.
BSPIL(I) = 0.0
INITIALIZE TSPIL TO DENSITY AT BEGINNING OF SPILL.
ALSO TREATED PORTION TO ZERO (TSPIL,SSPIL)
TSPIL(I) = DSPIL(I)
SSPIL(I) = 0.0
BSPIL(I) = 0.0
TSPIL(I) = 0.0
10 CONTINUE
IF (BPII2.EQ.0) GO TO 29
WRITE (80,260)
260 FORNAT (110,'-')/
29 CONTINUE
C
UPDATE THE SPILLET BORDER COUNTS.
BSPIL = JSPIL
C
END HERE
C
RETURN
C
CONTINUE
IF (LSPIL.EQ.0) RETURN
HERE IF THIS IS A RESTART
THIS SECTION READS THROUGH THE INPUT SPILLET'S WHICH
HAVE ALREADY BEEN ENTERED IN THE PREVIOUS RUN.
READ (80,100) BSTEP,DSPT,ESPT,SSPT,TSPT,
1 OSPT,USPT,ISPT,YSPT
READ (80,101) (CSPT(I),I=1,BSPIL)
WRITE (80,230) IIE
230 FORNAT (21,' AT STEP ',I4,' OLD SPILLET INFORMATION IS: ')
BSPIL = JSPIL
RETURN
END
SUBROUTINE SOBOP(I,T,B,BORDB,IST,BPRTS,BSPIL,BSHOR)
C
C THIS SUBROUTINE WRITES OUT TO THE DISK THE
C NECESSARY VARIABLES NEEDED TO RESTART A RUN IF A RUN
C IS INTERRUPTED. IT WRITES OUT THE INFORMATION EVEN
C CERTAIN NUMBER OF STEPS AS DEFINED BY BSTEP. EACH
C TIME THE OLD VALUES ARE WRITTEN OVER SO THAT ANY
C RESTART WILL HAVE TO START AT THE LAST STEP WHICH
C WAS WRITTEN OUT.
C
C .....
C COMMON /CBER/ SCBER, BCBER(10), DCBER(10), ECBER(10),
1 SCBER(10), TCBER(10), VCBER(10), BCBER(10), ICBER(10),
2 ECBER(10), PCBER(10)
COMMON /CLB/ BCLB, BCLB(10), DCLB(10), BCLB(10), BCLB(10),
1 VCLB(10), ICCLB(10), ICLB(10)
COMMON /SOB/ BSHOR, BSHU, BSHI, BSHL, BSHI, BSHL, BSHI, BSHL,
1 BSHI, BSHL, BSHI, BSHL, BSHI, BSHL, BSHI, BSHL,
COMMON /BPII/ BPII, BPII, BPII, BPII, BPII, BPII, BPII, BPII,
1 BPII, BPII, BPII, BPII, BPII, BPII, BPII, BPII,
COMMON /CSTL/ ISHOB, JSHOB, KSHOB, SPETA,
1 SPATC, DT, TIBI, TIRAB, ISCAL, USAV(99)
COMMON /BASS/ IBATB, IBIBO, IBBOT, IBCLB, IBDBP, IBLOS,
1 IBSHI, IBSHU, IBSSU
COMMON /ODTF/ BOSH, BUSH, BUCB, BDPY, BORS, BULT,
1 BDDP, BUVL
COMMON /SPIL/ BSPIL, BSPIL, ASPIL(99), BSPIL(99), DSPIL(99),
1 PSPIL(99), CSPIL(99,8), BSPIL(99), SSPIL(99),
2 TSPIL(99), YSPIL(99), OSPIL(99), BSPIL(99),
3 TSPIL(99), SSPIL(99), BAISSL
COMMON /PTP/ BCLASS, BUBSD(200), DDLAB(200), DDBRE(200),
1 DBASS(200), DVELL(200), DCOPB(200,8), BCLAS, BOCCL
C
DIMENSION STATEMENTS
DIREPSION I(BSHI), T(BSHI), B(BSHI)
INTEG=2 BORB(BSHI)
C
START HERE
C

```

Figure VII.-3. MAIN


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C CALCULATE AMOUNT OF MASS LOST BY SPILLET
C
C      BRAS = PREZPT*ASP
C      IF(SUBAS.GT.1850) BRAS=BRASOR
C      MSP = MSP - BRAS
C      BRAS = BRAS + SUBAS
C      BRSDS = BRSDS + SUBAS
C      BRSDP = BRSDP - BRSDS
C
C THIS SECTION COMPUTES THE APPROXIMATE AMOUNT
C OF MASS TO BE REPRESENTED BY EACH PARTICLE
C DURING EACH STEP OF THE PREVIOUS POP
C THIS VALUE IS THEN USED IN THE LOGIC BOX.
C IF(BRSDS.EQ.0) GO TO 90
C IF(1850.LT.BRSDP) GO TO 90
C BRSPAF = BRSDS/PILOT*(PBAR)
C TBT = TBT / 3600.0
C WRITE(99,100) TBT, BRSDS, BRSPAF, BRSDP
C FORMAT(21, /, 51, 'AT TIME TOTALS', P13.6, 'BOARDS',
1 /, 51, 'THIS RESULTS IN', P13.6, 'DROPS PER DROPLET SPREAD
2 OUT OVER', 15, 'PARTICLES')
3
90 CONTINUE
C
C      SUBROUTINE EWTB (ISPIL, I, T, Z, WORDS, SUBAS, INSPAF,
1      POBIS, BRSD)
C
C      SUBROUTINE DESCRIPTION
C
C      THIS SUBROUTINE INJECTS OIL DROPLETS INTO THE WATER COLUMN.
C
C
C      COBBOX STATEMENTS
C
C      COBBOX /DPTH/ NAIDI, NAIDI, AD, DPTH(30, 30), EDL, YDL,
1      IDS, YDS
C      COBBOX /IBUC/ DIBF, AFAC, BIFAC, BOFAC, DDIAF, DVELLT, BWT
C      COBBOX /CVAL/ INSP, JASUB, BRSD, BPTIC,
1      BPTIC, DT, TIRE, TIRAL, ISCAL, BSAT(99)
C      COBBOX /BASS/ IBATA, IBIC, IBDI, INCL, IBDIF, IBLOS,
1      IRSU, IRSD, IRSDS
C      COBBOX /PTIP/ BCLASS, BOBDD(200), DDIAF(200), DDIR(200),
1      BRASS(200), DVELL(200), DCOMP(20, 0), WTCLASS, BDECI
C      COBBOX /SPIL/ ASPIL, BSPIL, ASPIL(99), BSPIL(99), DSPIL(99),
1      PSPIL(99), GSPIL(99, 0), BSPIL(99), SSPIL(99),
2      TSPIL(99), YSPIL(99), OSPIL(99), ISPIL(99),
3      TSPIL(99), SSPIL(99), BAIISP
C      COBBOX /SDES/ STIARS, ISDE, BRIT, BRAT, BRAT, DI, DT, DZ,
1      IORIC, TORIC, SORIC
C
C      DIMENSION STATEMENTS
C
C      DIMENSION DCOMP(8)
C      DIMENSION I(BRAT), T(BRAT), Z(BRAT)
C      INTEGER*2 WORDS(BRAT)
C
C      DATA STATEMENTS
C
C      DATA BRD1, BO, BV, 0, 2, 4/
C
C      DO NOT CREATE PARTICLES IF THIS IS A SHORT BOX
C
C      IF(BRSD.EQ.1) RETURN
C
C      THE AMOUNT OF MASS PER PARTICLE HAS BEEN DETERMINED
C      IN A PREVIOUS SUBROUTINE BOX
C
C      IF(BRSDS.LT.0.0) RETURN
C      IF(ISCAL.EQ.2) BO = 5
C
C      DETERMINE THE NUMBER OF PARTICLES
C
C      PART = SUBAS /BRSPAF
C      SPART = PART * 0.5
C
C      S Y A R T = B I E E
C
C      RETURN IF NO ESTABLISHMENT
C
C      IF(SPART.LT.0) RETURN
C
C      DETERMINE THE PARTICLE PROPERTIES FOR THIS SPILLET
C
C      DDIR(1) = DSPIL(1850)
C      DO 10 IPRAC = 1, 8
C      DCOMP(IPRAC) = GSPIL(1850, IPRAC) *
10 CONTINUE
C
C      DOES A CLASS ALREADY EXIST WITH THESE PROPERTIES.
C
C      IF(BCLASS.EQ.0) GO TO 30
C      DO 20 ICLASS=1, BCLASS
C      IF(DDIAF(1).NE.DDIR(ICLASS)) GO TO 20
C      IF(DDIAF(2).NE.DDIR(ICLASS)) GO TO 20
C      IF(DVELLT(1).NE.DVELL(ICLASS)) GO TO 20
C      DO 25 IPRAC=1, 8
C      IF(DCOMP(IPRAC).NE.DCOMP(ICLASS, IPRAC)) GO TO 20
25 CONTINUE
C
C      IS THERE ANY ROOM IN THIS CLASS FOR MORE PARTICLES?
C
C      BPT = BOBDD(ICLASS) * SPART
C      IF(BPT.GE.BONCL) GO TO 20
C      JCLASS = ICLASS
C      GO TO 30
20 CONTINUE
C
C      CONTROL CODES HERE IF A NEW CLASS IS TO BE CREATED CHECK THAT
C      SOME OF THE EXISTING CLASSES ARE EMPTY.
C
C      DO 40 ICLASS=1, BCLASS
C      IF(BOBDD(ICLASS).GT.0) GO TO 40
C      JCLASS = ICLASS
C      GO TO 55
40 CONTINUE
C
C      CHECK THAT THERE IS ROOM FOR A NEW CLASS. IF NOT CORRECT AND PUT
C      ALL NEW PARTICLES TO BE INJECTED INTO THE LAST CLASS: BCLASS.

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```

C
C      JCLASS = BCLASS
C      IF(BCLASS.LT.BTCLASS) GO TO 30
C      IF(BDIS.EQ.1) GO TO 30
C      BDIS = 1
C      WRITE(99,100) BCLASS
100 FORMAT(21, 5(' '), ' SC ROOM FOR A NEW CLASS. ALL NEW
1 PARTICLES WILL BE PUT INTO CLASS:', 15/)
C      GO TO 30
50 CONTINUE
C      BCLASS = BCLASS + 1
C      JCLASS = BCLASS
C
C      HERE TO SAY PARTICLE PROPERTIES FOR JCLASS.
C
C      CONTINUE
55 BDIR(JCLASS) = DDIR(1)
C      BDIR(JCLASS) = DDIR(1)
C      DVELL(JCLASS) = DVELL(1)
C      DO 60 IPRAC=1, 8
C      DCOMP(JCLASS, IPRAC) = DCOMP(IPRAC)
60 CONTINUE
C
C      THE CLASS HAS BEEN DETERMINED AND THE DROPLET PARAMETERS SAID
C
C      CONTINUE
30 CONTINUE
C
C      DO THESE ADDITIONAL PARTICLES EXCEED THE TOTAL PARTICLE COUNT?
C
C      BTERP = BRAT + SPART
C      IF(BTERP.LT.BRAT) GO TO 90
C      BPART = BRAT - BRAT
C
C      CHECK THAT THE BALANCE # OF PARTICLES HAS NOT BEEN EXCEEDED
C
C      IF(BPART.GT.0) GO TO 90
C      WRITE(99,120) BRAT
120 FORMAT(21, 5(' '), ' NO NEW PARTICLES MAY BE ADDED',
1 ' THIS STEP.', 15, ' PARTICLES HAVE ALREADY BEEN CREATED.//')
C      RETURN
90 CONTINUE
C      BLOF = BRAT + 1
C      BUPF = BRAT - SPART
C
C      CALCULATE THE RADII RESTRICTIONS ON PARTICLE INJECTION
C
C      BO = BSPIL(1850) / BIFAC
C      A = BO / (AFAC * BIFAC)
C      BRAT = (BSPIL(1850) * (1.0 - ((NEST * (3600.0**2) / 5.0) /
1 (BOPAC*(TIRE*TIRE)-(BSPIL(1850)*BSPIL(1850))))))
C      D = SQRT(BO/A)
C      B = (BRAT - BO) / (1.0 - D)
C      C = (SC - BRAT + D) / (1.0 - D)
C
C      DETERMINE THE CENTER OF THE PARTICLE DISTRIBUTION IF I AM 1.
C
C      CALL DIST(EDL, YDL, ISPIL(1850), TSPIL(1850),
1      BO, AD, D, IC, YC)
C      IC = IC/TDS + 1.0
C      YC = YC/YDS + 1.0
C
C      IF THIS IS THE FIRST PASS THROUGH EWTB DEFINE THE ORIGIN
C      NOTE: THE SUBSURFACE PROGRAMS HAVE NOT BEEN CALLED SO A FLOATING
C      ORIGIN HAS NOT BEEN DEFINED. DEFINE THE ORIGIN OF THE FLOATING
C      GRID HERE. THIS ORIGIN WILL BE USED BY GRIDER WHEN THE
C      SUBSURFACE PROGRAMS ARE CALLED.
C
C      IF(BLOF.EQ.1) GO TO 210
C      BORG = IC - DI * FLOF(BRSD) / (2.0 * TDS)
C      YORG = YC - DT * FLOF(BRSD) / (2.0 * TDS)
C      BORG = 0.0
210 CONTINUE
C
C      INJECT PARTICLES.
C
C      CALL INJECT(IC, YC, BO, A, B, C, I, T, Z, WORDS,
1      BLOF, BOPF, JCLASS, POBIS)
C
C      MASS BALANCE THIS STEP.
C
C      BRASS(JCLASS) = SUBAS/PILOT*(PBAR)
C      BOBDD(JCLASS) = BOBDD(JCLASS) + SPART
C      BRAT = BOF
C
C      E T O B B I E E
C
C      RETURN
C
C      SUBROUTINE EYPOB(ISP, OLDIAD, DAGES, DVEL)
C
C      THIS SUBROUTINE WILL PREDICT EVAPORATION LOSS FROM THIS
C      SPILLET FOR ONE TIME STEP. TO ACCOMPLISH THIS THE OIL IS
C      BROKEN UP INTO EIGHT FRACTIONS AND THE LOSS DUE TO EVAPORATION
C      IS CALCULATED FOR EACH FRACTION AND THEN SUMMED FOR THE ENTIRE
C      AS A WHOLE. SINCE THE DECAY "CONSTANT" IS NOT CONSTANT WITH
C      TIME THE TIME STEP IS DIVIDED INTO SEVERAL SUB TIME STEPS.
C      THE "CONSTANT" IS THEN ASSUMED TO BE CONSTANT FOR THESE SUBSTEPS
C      AND THE EVAPORATION LOSS CALCULATED FOR THE SUBSTEP. THE LOSS
C      IS THEN ACCUMULATED FOR THE ENTIRE TIME STEP.
C
C      VARIABLE DESCRIPTION
C
C      ABSERO - ABSOLUTE ZERO (DEGREES CENTIGRADE).
C      ABRA - OF SPILLET (METERS**2).
C      COB1 - ARRAY OF CONSTANTS.
C      COB2 - ARRAY OF CONSTANTS.
C      COB3 - ARRAY OF CONSTANTS.
C      DAGES - TEMPERATURE (DEGREES CENTIGRADE).
C      RAD - RADIUS OF SPILLET AT SUBSTEP TIME (METERS).
C      DELTA - TIME OF SUBSTEP IN THE INTEGRATION PROCEDURE (SEC).
C      DT - TIME STEP IN THE MAIN PROGRAM (SEC).
C      NIST - # OF STEPS IN THE INTEGRATION PROCEDURE.
C      OLDIAD - RADIUS OF SPILLET AT LAST TIME STEP (METERS).
C      P - VAPOUR PRESSURE.
C      Q - CONSTANT.
C      R - CONSTANT.
C      SC - GAS CONSTANT.
C      DVEL - WIND VELOCITY (M/SEC).

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Figure VII.-3. MAIN

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C
C
C      COMMON STATEMENTS
C
C      COMMON /DESS/ DEB(8)
C      COMMON /CSTL/ INSD, JSD, HSD, SPSTA,
C      /SPSTC, DT, TIME, TIRAL, ISCAL, BSAT(99)
C      COMMON /BASS/ IBATE, IBIO, IBROT, IBCLR, IBDRF, IBLOS,
C      IBSR, IBSD, IBSDS
C      COMMON /SPIL/ SPIL, DSPIL(99), MSPIL(99), DSPIL(99),
C      1 SPIL(99), GSPIL(99), HSPIL(99), SSPIL(99),
C      2 SPIL(99), TSPIL(99), GSPIL(99), HSPIL(99), SSPIL(99),
C      3 SPIL(99), MSPIL(99), MSPIL
C
C      DIMENSION STATEMENTS
C
C      DIMENSION COB1(7), COB2(7), COB3(7)
C
C      DATA STATEMENTS
C
C      DATA COB1/ 1617.61, 1825.03, 1861.79, 1893.78, 1807.34,
C      1 1801.00, 1789.85/
C      DATA COB2/ 202.174, 149.757, 204.697, 151.822, 206.479,
C      1 162.771, 166.560/
C      DATA COB3/ 6.9357, 7.0107, 6.9111, 6.9871, 6.9054,
C      1 6.9698, 6.9696/
C      DATA CONST, Q, B, RC/ 49.0, 0.42, -0.055, 8.31399/
C      DATA BNS24C, PI/ 273.0, 3.14159/
C      DATA BINT/ 10/
C
C      S T A B T H E E P E
C
C      IF (HNSDA LE D.O) RETURN
C      BPA = 7
C      BPAAC = BPA * 1
C      BRCIG = DSPIL(ISP) / TSPIL(ISP)
C      DELTA = DT / (FLOAT(BINT) * 3600.0)
C      DSPIL(ISP) = 0.0
C      DB = (MSPIL(ISP) - OLDDB) / FLOAT(BINT)
C      GSDX = 0.0
C      GSDO = 0.0
C      TRAS = GSPIL(ISP, 8)
C      DO 10 IFAAC = 1, BPA
C      TRAS = TRAS + GSPIL(ISP, IFAAC)
C      COEFS = 0.0
C      BQ = OLDDB - DB / 2.0
C      DO 20 J = 1, BNS
C      BQ = BQ + DB
C      AREA = PI * BQ * BQ
C      P = 10.0 * (COB1(IFAAC) - COB1(IFAAC) / (COB2(IFAAC)
C      * DAGRES1))
C      1 COEF = CONST * EXP(0*BVEL) * (1.0 / (AREA**(-B)))
C      COEF = COEF * P / (IC * (ABS(EO) + DAGRES1))
C      COEFS = COEFS + COEF
C      20 CONTINUE
C      IF (REGIN GT 2.0078) COEFS = COEFS / 5.0
C      BZOB = COEFS * DELTA
C      IF (IZOBL LT 20) .AND. (GSPIL(ISP, IFAAC) GT 10.0E-6) 1
C      GO TO 30
C      GSPIL(ISP, IFAAC) = 0.0
C      GO TO 40
C
C      30 CONTINUE
C      GSPIL(ISP, IFAAC) = GSPIL(ISP, IFAAC) * EXP(-BZOB)
C      CONTINUE
C      GSDO = GSDO + GSPIL(ISP, IFAAC) / DEB(IFAAC)
C      10 CONTINUE
C      GSDO = GSDO + GSPIL(ISP, 8)
C      GSDO = GSDO + GSPIL(ISP, 8) / DEB(8)
C
C      CALCULATE THE DENSITY OF THE OIL IN THIS SPILLET.
C      GSDO IS THE MASS OF SOME QUANTITY OF OIL.
C      GSDO IS THE VOLUME OF THE SAME QUANTITY OF THIS OIL.
C
C      DSPIL(ISP) = GSDO / GSDO
C
C      MASS OF OIL EVAPORATED FROM THIS SPILLET
C      ENAS = MSPIL(ISP) * (TRAS - GSDO) / TRAS
C      IF (ENAS GT MSPIL(ISP)) ENAS = MSPIL(ISP)
C      ENATE = ENAS * IBATE
C      ENSD = ENSD + ENAS
C      MSPIL(ISP) = MSPIL(ISP) - ENAS
C
C      E N D M E E P E
C
C      RETURN
C
C      SUBROUTINE INJECT(IC, IC, RO, A, B, C, E, I, Z,
C      1 BORDS, BLOS, SUPR, JCLASS, PORIN)
C
C      SUBROUTINE DESCRIPTION
C
C      THIS SUBROUTINE IS USED TO DETERMINE THE LOCATION OF THE
C      ESTIMATED PARTICLES. THE DISTRIBUTION WILL BE UNIFORM
C      IF I AND J WITHIN RC OF THE CENTER AND THEY FALL OFF LINEARLY
C      FROM RD TO BHAL AT BHAL THE DISTRIBUTION GOES TO ZERO.
C      THE DISTRIBUTION IS UNIFORM IN X BETWEEN RL AND RU
C
C      .....
C
C      COMMON STATEMENTS
C
C      COMMON /CORP/ BAICR, BAICX, BC, BCOMP(30, 30), BCL, BCL,
C      1 BCS, BCS
C      COMMON /DPTH/ BARDX, BARDY, BD, BDEPTH(30, 30), BDL, BDL,
C      1 BDS, BDS
C      COMMON /IBJC/ BIPC, BIPAC, BIPAC, BOPAC, BDIABT, BVELST, BSEP
C      COMMON /IBS/ BIAS, BBS, BBITA, BBAI, BBAI, BDI, DT, DI,
C      1 BDI, BDI, BDI, BDI
C      COMMON /CSTL/ INSD, JSD, HSD, SPSTA,
C      1 SPSTC, DT, TIME, TIRAL, ISCAL, BSAT(99)
C
C      DIMENSION BAP(3)
C      BHAL = 1(BBAI), Y(BBAI), Z(BBAI)
C      ISTRGB = 2 BORDS(BBAI)
C
C      DATA STATEMENTS
C
C      DATA TROPI, BPASS/ 6.28319, 0/
C      DATA FIVE, BU/ 5.0, 6/
C
C      S T A B T H E E P E
C
C      INITIALIZE THE SEED FOR THE RANDOM NUMBER GENERATOR
C
C      IF (BPASS EQ 1) GO TO 10
C      BPASS = 1
C      IS = 5 * 15
C      IS = 7810666
C      IS = 2 * IS
C      10 CONTINUE
C
C      CALCULATE THE RANGE OF RANDOM NUMBERS CORRESPONDING
C      TO PARTICLES WITHIN RC.
C
C      BLIN = SORT (RC / R)
C
C      DO LOOP OVER PARTICLES TO BE CREATED.
C
C      DO 1 B = BLOS, BOPS
C      JJ = 0
C      CONTINUE
C
C      2 OBTAIN RANDOM NUMBERS.
C
C      CALL RAND(IJ, IO, P, B1)
C      CALL RAND(IJ, IO, P, B2)
C      CALL RAND(IJ, IO, P, B3)
C
C      CALCULATE PARTICLE DISTANCE AND ANGLE FROM SPHERE CENTER
C
C      IF (B1 LE BLIN) RADIUS = A * B1 * B1
C      IF (B1 GT BLIN) RADIUS = B * B1 * C
C      TRETA = TRCPI * B2
C      DOR1 = RADIUS * SIN(TRETA)
C      DOR2 = RADIUS * COS(TRETA)
C
C      IF LARGE SCALE MODE IS USED, POSITIONS ARE CONVERTED TO DECILES
C
C      IF (BLOS EQ 0) DOR1 = 0.0
C      IF (BLOS EQ 0) DOR2 = 0.0
C      IF (ISCAL EQ 1) GO TO 79
C      SCAL = 6371.0 * 1000.0 * 3.14159 / 180.0
C      BQ = 3.14159 / 180.0
C      DOR2 = DOR2 / SCAL
C      TLAT = (IC * D5) * (BDL * B3) * DOR2
C      DOR1 = DOR1 / (SCAL * COS(TLAT * B3))
C      CONTINUE
C
C      79 CALCULATE THE PARTICLE POSITION IN X AND Y.
C
C      X(B) = (IC - IORIC) * B3 + DOR1
C      Y(B) = (IC - IOIC) * B3 + DOR2
C
C      CHECK THAT THE PARTICLE FALLS IN THE PILED GRID.
C
C      I1 = X(B) / BDS + IORIC
C
C      B1 = I1
C      B0 = B1 + 1
C      B1 = Y(B) / BDS + IOIC
C      B1 = Y1
C      B0 = B1 + 1
C      JJ = JJ + 1
C      IF (JJ LT 100) GO TO 800
C      WRITE (BU, B01)
C      801 POPRAT(21, 1) SEE PARTICLE POSITIONS ARE OUT OF PILED GRID
C
C      800 CONTINUE
C      IF ((B0 GT BARDX) .OR. (B0 GT BARDY)) GO TO 2
C      IF ((B1 LT 1) .OR. (B1 LT 1)) GO TO 2
C      IF ((BCORP(B0, B0), EQ 0) .OR. (BCORP(B0, B1), EQ 0)) GO TO 2
C      IF ((BCORP(B1, B0), EQ 0) .OR. (BCORP(B1, B1), EQ 0)) GO TO 2
C
C      IS THE SPACING BETWEEN THE FIRST PARTICLES BROAD?
C
C      IF (B DS 2) GO TO 790
C      BDI = ABS(2(1) - 1(2))
C      BDI = ABS(1(1) - 1(2))
C      IF (ISCAL EQ 1) GO TO 791
C      BDI = BDI * SCAL
C      BDI = BDI * SCAL * COS(TLAT * B3)
C      791 CONTINUE
C      IF ((BDI LT PORIN) .OR. (BDI LT PORIN)) GO TO 2
C      790 CONTINUE
C
C      CALCULATE THE Z POSITION OF THE PARTICLE.
C
C      Z(B) = DEPC + FIVE * (B2 - 0.5)
C
C      SAVE THE CLASS TO WHICH THIS PARTICLE BELONGS.
C
C      BORDS(B) = JCLASS
C
C      PRINT OUT THE PARTICLE POSITION.
C
C      1 CONTINUE
C
C      B E T U R N
C
C      RETURN
C      BND
C      SUBROUTINE LOCB(BCAD, BI, B1, BRC, IL, IS, IS, VS, VARI,
C      1 VAL2, IC, IC, A, VAL1, VAL2, BDLSPIL, ISFIL)
C
C      THIS SUBROUTINE FINDS THE SEPARATION IN DEGREES IN LONGITUDE
C      AND IN LATITUDE BETWEEN THE ORIGIN OF THE GIVEN COORDINATE
C      SYSTEM AND THE GIVEN POINT. THIS LINE IS THEN ROTATED INTO
C      THE GIVEN COORDINATE SYSTEM, I.E., THE SEPARATION PARALLEL
C      TO THE COORDINATE SYSTEM Y AXIS AND THE SEPARATION PARALLEL
C      TO THE COORDINATE SYSTEM X AXIS. FINALLY ALL GRID ELEMENTS
C      WHICH COVER THE CIRCLE OF RADIUS R CENTERED ON THE GIVEN POINT
C      ARE AVERAGED AND THE AVERAGES ARE RETURNED.
C
C      .....
C
C      COMMON STATEMENTS

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Figure VII.-3. MAIN

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CORROD /CUTL/ ISSUB, JNSUB, ERSUB, BRPTA,
1  BRPTC, DT, TIBL, TIBRAZ, ISCAL, BSAB(99)
C
C      DIMENSION STATEMENTS
C
DIMENSION VAR1(30, 30), VAR2(30, 30)
C
C      DATA STATEMENTS
C
DATA P1, B0, B0/ 3.16159, 6, 2/
IF(ISCAL.EQ.2) B0 = 5
BLSPL = 0
C
C      S T A R T   H E R E
C
IF ONLY ONE GRID ELEMENT HAVE THE VALUE AND RETOBS.
C
IF (B1.GT.1) .OR. (B1.GT.1) GO TO 10
VAL1 = VAR1(1, 1)
IF (B2.EQ.2) VAL2 = VAR2(1, 1)
BETOPF
CONTINUE
10
C
C      FIND THE LOCATION OF THE SPILLET CENTER IN THE GRID
C      IF NECESSARY ROTATE THE DISTANCE
C
CALL DIST(XL, YL, XC, YC, B0, ANG, D, IDT, YDT)
C
C      FIND THE SPILLET LIMITS IN THE GRID
C
BT = 1
BT = 8
IF (ISCAL.EQ.1) GO TO 85
20 SCAL = 6371.0*1000./RUC.0
PI = B/(SCAL*COS(IC/57.296))
BT = B/SCAL
85
CONTINUE
IDL = IDT - BT
IDU = IDT + BT
YDL = YDT - BT
YDU = YDT + BT
C
C      OBTAIN ALL OF THE GRID ELEMENTS IMMEDIATELY ADJACENT TO THE
C      SPILLET OR IS IT.
C
BIL = IDL / IS + 1.0
BIO = IDU / IS + 2.0
BIL = YDL / IS + 1.0
BIO = YDU / IS + 2.0
VAL1 = 0.0
VAL2 = 0.0
C
C      CHECK THAT THE SPILLET LIES WITHIN THE STUDY AREA.
C
IF (B1.GT.0) GO TO 80
IF (B1.GT.0) GO TO 41
CONTINUE
45
BLSPL = 1
WRITE(BR, 200) ISPL
200 FORMAT(2X, ' SPILLET ', J4, ' IS COMPLETELY OUT OF RANGE')
C
C
C
C      RETOBS
C      CONTINUE
C      BIL = 1
40
CONTINUE
IF (B1.LI.B1) GO TO 50
IF (B1.GT.B1) GO TO 45
BIO = B1
50
CONTINUE
IF (B1.GT.0) GO TO 60
IF (B1.LI.0) GO TO 45
BIL = 1
60
CONTINUE
IF (B1.LI.B1) GO TO 70
IF (B1.GT.B1) GO TO 45
BIO = B1
70
CONTINUE
C
C      AVERAGE VARIABLES OVER THE APPROPRIATE GRID ELEMENTS.
C
DO 20 BI=BIL, BIO
DO 30 BJ=BIL, BIO
VAL1 = VAL1 + VAR1(BI, BJ)
IF (B2.EQ.2) VAL2 = VAL2 + VAR2(BI, BJ)
30
CONTINUE
20
CONTINUE
BIOB = FLOAT((BIO-BIL+1) * (BIO-BIL+1))
VAL1 = VAL1 / BIOB
IF (B2.EQ.2) VAL2 = VAL2 / BIOB
C
C      E N D   H E R E
C
C
C      RETOBS
C      ETC
C      SUBROUTINE AARD(II, IO, P, YIO)
C      IO=IO*10
C      YIO=IO/P* 0.5
C      RETOBS
C      ETC
C      SUBROUTINE EROB( DDB, BEC, DDB, BEB, BVAR)
C
C      THIS SUBROUTINE IDENTIFIES THOSE EFFORTS TO CLEANUP
C      OR TO TREAT THE SPILLERS WHICH HAVE EXPIRED. THE LIST OF
C      EFFORTS IS THEN COMPRESSED REMOVIING EXPIRED ONES.
C
C
C
C      .....
C
C      COMMON STATEMENTS
C
CORROD /CUTL/ ISSUB, JNSUB, ERSUB, BRPTA,
1  BRPTC, DT, TIBL, TIBRAZ, ISCAL, BSAB(99)
C
C      DIMENSION STATEMENTS
C      DIMENSION DDB(10, BVAR), BEC(10), DDB(10)
C
C
C      S T A R T   H E R E
C
FIND ALL EXPIRED EFFORTS.
JTEMP = 0

```

```

DO 50 JTEMP=1, BEC
BECT = BEC(JTEMP) + 3600 0
DDBT = DDB(JTEMP) + 3600 0
BBD = BEC + DDBT
IF (BBD.GT.100) GO TO 50
JTEMP = JTEMP + 1
BSAB(JTEMP) = JTEMP
50
CONTINUE
REORDER THE CLEANUP LIST SO THAT EXPIRED EFFORTS ARE AT THE END
C
IF (JTEMP.EQ.0) RETOBS
JTEMP = BEC + 1
JTEMP = JTEMP + 1
DO 70 JTEMP=1, JTEMP
JTEMP = JTEMP - 1
ETEF = ETEF - 1
LTEMP = BSAB(JTEMP)
IF (LTEMP.EQ.0) GO TO 70
DO 80 I=1, BVAR
DDB(LTEMP, I) = DDB(BTEMP, I)
80
CONTINUE
70
CONTINUE
REOBS EXPIRED EFFORTS AND RETOBS.
C
BEC = JTEMP - 1
C
E N D   H E R E
C
C
C      RETOBS
C      ETC
C      SUBROUTINE SPREAD( ISPL)
C
C      THIS SUBROUTINE SPREADS A SPILLET FOR ONE TIME STEP. THE
C      SPREADING PROCEDURE USED IS THAT DEVELOPED BY FAY FIRST HOWEVER
C      THE "STARTING TIME" OF THE SPILLET MUST BE DETERMINED FROM
C      ITS RADIUS AND ITS POLDS. THEN THE REGIME IS DETERMINED
C      AND FINALLY THE SEA RADIIUS AFTER ONE TIME STEP. THIS APPROACH
C      MUST BE TAKEN AS THE VOLUME CHANGES FROM STEP TO STEP.
C
C      VARIABLE DESCRIPTION
C
CORF1 - SPREADING COEFFICIENT FOR FIRST REGIME.
CORF2 - SPREADING COEFFICIENT FOR SECOND REGIME.
CORF3 - SPREADING COEFFICIENT FOR THIRD REGIME.
DELTA - (WATER DENSITY - OIL DENSITY) / WATER DENSITY.
GRAV - GRAVITATIONAL ACCELERATION (CM/SEC**2).
RAD - RADIUS OF SPILLET (CM).
BSOB - DENSITY OF SEA WATER (GB/CC).
BRAD1 - RAI RADIIUS TO WHICH A SPILLET OF THIS VOL WILL SPREAD.
SIC - SPREADING TENSION (DYNES/CM*GB/SEC**2).
TIBJ - TIME AT WHICH THE SPILLET GOES FROM REGIME 1 TO
REGIME 2.
VISH20 - VISCOSITY OF SEA WATER (STORES*CM**2/SEC).
VISH20 - SQRT(VISH20).
VBI8 - BALLBOB VOLUME FOR WHICH PAYS REGIME 2 IS SKIPPED.
VOL - VOLUME OF SPILLED OIL (CC).
C
C
C
C
C      .....
C
C      COMMON STATEMENTS
C
CORROD /CUTL/ ISSUB, JNSUB, ERSUB, BRPTA,
1  BRPTC, DT, TIBL, TIBRAZ, ISCAL, BSAB(99)
CORROD /SPIL/ BSPL, BSPL, BSPL(99), BSPL(99), BSPL(99),
2  SPIL(99), SPIL(99), SPIL(99), SPIL(99), SPIL(99),
3  SPIL(99), SPIL(99), BSAPL
C
C      DATA STATEMENTS
C
DATA P1/ 3.16/
DATA BBOB/ 1.024/
DATA VISH20/ 0.012077/
DATA CORF1, CORF2, CORF3/ 1.16, 1.45, 2.30/
DATA GRAV/ 980.5416/
C
C      S T A R T   H E R E
C
BPRC = 0.0
VISH20 = SQRT(VISH20)
I3 = DT
C
C      CALCULATE TEMPORARY VARIABLES.
C
DELTA = (BSOB - DSPIL(ISPL)) / BBOB
VOL = BSPL(ISPL) * 1.0E+6 / DSPIL(ISPL)
RAD = BSPL(ISPL) * 100.0
C
C      IF THE SPILLET HAS REACHED ITS BALLBOB SIZE: NAME
C      THE RADIIUS THE BALLBOB SIZE AND RETOBS
C
BFA = 1.0E5 * (VOL / 1.0E6)**.75
BRAD = SQRT(BFA / P1) * 100.0
IF (BRAD.GT. RAD) GO TO 79
BAC = BRAD
C
C      RETOBS
C
C      FIND THE FRACTION OF THIS SPILLET WHICH HAS BEEN CHEMICALLY
C      TREATED AND WEIGHT THE INTERFACIAL TENSION ACCORDINGLY.
C
79
IF (BSPL(ISPL).GE.1.0) GO TO 10
IF (BSPL(ISPL).LI.0.0) GO TO 11
FRAC = BSPL(ISPL)
SIG = BSPL(ISPL) * (1.0 - FRAC) + SSPLT(ISPL) * FRAC
GO TO 20
CONTINUE
SIG = BSPL(ISPL)
GO TO 20
CONTINUE
SIG = SSPLT(ISPL)
20
CONTINUE
C
C      IF THE SPILLET IS TOO SMALL THE SECOND REGIME WILL BE SKIPPED
C      DETERMINE IF THIS IS THE CASE FOR THIS SPILLET.
C
VBI8 = (CORF2 + CORF3)**6 / (CORF1**12)
TRAP = VISH20 * DELTA * GRAV
VBI8 = VBI8 * (SIG / BSOB)**3 / (TRAP**2)

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Figure VII.-3. MAIN

```

IF (VOL.CT VBR) GO TO 40
DETERMINE THE TIME SINCE THE START OF THE SPILLET
ASSUMING THAT IT IS IN THE FIRST REGIME.
T1 = ((RAD / COEF1)**2) / SQRT(DELTA * GRAV * VOL)
T1 = T1 * DT
DETERMINE THE TIME AT WHICH THE SPILLET GOES FROM THE FIRST
REGIME TO THE THIRD REGIME.
T13 = DELTA * GRAV * VOL * VISB20
T13 = T13 * ((RHO6 / SIG)**2)
T13 = ((COEF1 / COEF3)**4) * T13
IS THE SPILLET IN THE FIRST REGIME?
IF (T1.LE.T13) GO TO 30
GO DIRECTLY TO 50 IF THIS IS THE FIRST TIME STEP.
IF (RAD.LE.0.0) GO TO 50
DETERMINE THE TIME SINCE THE START OF THE SPILLET
ASSUMING THAT IT IS IN THE THIRD REGIME.
T3 = ((SIG / RHO6)**2) / VISB20
T3 = ((RAD / COEF3)**4) / T3**((1.0/3.0)
T3 = T3 * DT
GO TO 50
DETERMINE THE TIME SINCE THE START OF THE SPILLET
ASSUMING THAT IT IS IN THE FIRST REGIME.
CONTINUE
T1 = ((RAD / COEF1)**2) / SQRT(DELTA * GRAV * VOL)
T1 = T1 * DT
DETERMINE THE TIME AT WHICH THE SPILLET GOES FROM THE FIRST
REGIME TO THE SECOND REGIME.
T12 = VOL / (DELTA * GRAV * VISB20)
T12 = ((COEF2 / COEF1)**4) * (T12**((1.0/3.0))
IS THE SPILLET IN THE FIRST REGIME?
IF (T1.LE.T12) GO TO 30
DETERMINE THE TIME SINCE THE START OF THE SPILLET
ASSUMING THAT IT IS IN THE SECOND REGIME.
T2 = (DELTA * GRAV * (VOL**2) / VISB2)**((2.0/3.0)
T2 = ((RAD / COEF2)**4) / T2
T2 = T2 * DT
DETERMINE THE TIME AT WHICH THE SPILLET GOES FROM THE SECOND
REGIME TO THE THIRD REGIME.
T23 = DELTA * GRAV * VOL * VOL * VISB20
T23 = ((COEF2 / COEF3)**2) * (T23**((1.0/3.0)) * (RHO6 / SIG)
IS THE SPILLET IN THE SECOND REGIME?
IF (T2.LE.T23) GO TO 40
GO DIRECTLY TO 50 IF THIS IS THE FIRST TIME STEP
IF (RAD.LE.0.0) GO TO 50
DETERMINE THE TIME SINCE THE START OF THE SPILLET
ASSUMING THAT IT IS IN THE THIRD REGIME.
T3 = ((SIG / RHO6)**2) / VISB20
T3 = ((RAD / COEF3)**4) / T3**((1.0 / 3.0)
T3 = T3 * DT
CALCULATE THE SPILLET RADII IF IT IS IN THE THIRD REGIME.
CONTINUE
TEMP = ((SIG / RHO6)**2) * (T3**3) / VISB20
RAD = COEF3 * (TEMP**0.25)
GO TO 70
CALCULATE THE SPILLET RADII IF IT IS IN THE SECOND REGIME.
CONTINUE
TEMP = DELTA * GRAV * (VOL**2) * (T2**1.5) / VISB2
RAD = COEF2 * (TEMP**((1.0/6.0))
GO TO 70
CALCULATE THE SPILLET RADII IF IT IS IN THE FIRST REGIME.
CONTINUE
TEMP = DELTA * GRAV * VOL * (T1**2)
RAD = COEF1 * (TEMP**0.25)
BEH TO RECALCULATE THE AREA OF THE TREATED SPILLET ASSUMING
THAT THE TREATED FRACON SPREADS WITH THE REST OF THE SPILLET.
CONTINUE
ASPIL(ISPIL) = FRAC * PI * (RAD**2) * 1.0E4
IF (RAD.CT FRAC) RAD = RAD
RSPIL(ISPIL) = RAD / 100.0
END B E E E
RETURN
END
SUBROUTINE SBADPT(XC, YC, URIND, VRIND, UCBBT, VCBBT)
THIS SUBROUTINE MOVES THE CENTER OF MASS OF THE GIVEN SPILLET
FOR ONE TIME STEP. THE CURRENT VELOCITY OF THE SUBROUTINE
WILL MOVE THE SPILLET AT 3.5% OF THE WIND SPEED IN THE DIRECTION
OF THE WIND.
.....
COMMON STATEMENTS
COMMON /CUTL/ INSD, JNSD, EASD, SPRTA,

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```

1  SPPTC, DT, TIME, TIRNA, ISCAL, BSAT(99)
COMMON /SPIL/ BSPIL, RSPIL, ASPIL(99), RSPIL(99), DSPIL(99),
1  PSPIL(99), CSPIL(99), RSPIL(99), ASPIL(99), DSPIL(99),
2  TSPIL(99), TSPILT(99), RSPIL(99), RSPIL(99), RSPIL(99),
3  RSPIL(99), RSPILT(99), RASPL
DATA STATEMENTS
DATA PI, WINDP/ 3.14159, 0.035/
START B E E E
SCALE=PI*1000.0*6371.0/100.0
IF (ISCAL.EQ.1) GO TO 43
IF ON A LARGE SCALE, CONVERT DEGREES/SEC TO M/SEC.
VCBBT=VCBBT*SCALE
UCBBT=UCBBT*SCALE*COS(PI/57.296)
CONTINUE
CALCULATE THE DISTANCE MOVED IN X AND IN Y.
EDIST = DT * (URIND * WINDP * UCBBT)
YDIST = DT * (VRIND * WINDP * VCBBT)
CALCULATE THE LONGITUDE AND LATITUDE OF THE SPILL CENTER.
XC = XC + EDIST / SCALE
YC = YC + YDIST / SCALE
END B E E E
RETURN
END
SUBROUTINE TREAT(ISP, SDIAS)
THIS SUBROUTINE HANDLES THE CHEMICAL TREATMENT OF THE
OIL SPILLS.
.....
COMMON STATEMENTS
COMMON /CBER/ UCBER, UCBER, UCBER(10), UCBER(10), UCBER(10),
1  UCBER(10), UCBER(10), UCBER(10), UCBER(10), UCBER(10),
2  UCBER(10), UCBER(10), UCBER(10), UCBER(10), UCBER(10),
COMMON /CUTL/ INSD, JNSD, EASD, SPRTA,
1  SPPTC, DT, TIME, TIRNA, ISCAL, BSAT(99)
COMMON /RASS/ RASD, RASD, RASD, RASD, RASD, RASD, RASD,
1  RASD, RASD, RASD, RASD, RASD, RASD, RASD, RASD, RASD,
COMMON /SPIL/ BSPIL, RSPIL, ASPIL(99), RSPIL(99), DSPIL(99),
1  PSPIL(99), CSPIL(99), RSPIL(99), ASPIL(99), DSPIL(99),
2  TSPIL(99), TSPILT(99), RSPIL(99), RSPIL(99), RSPIL(99),
3  RSPIL(99), RSPILT(99), RASPL
DIMENSION STATEMENTS
DIMENSION DUB(10,10)
EQUIVALENCE (DUB(1,1),UCBER(1))
DATA STATEMENTS
DATA PI, W/ 3.14159, 6/
START B E E E
IF (UCBER.CT.0) GO TO 50
TBI = TIME / 3600.0
WRITE (80,210) TBI
FORNAT(10,0) AREAS UNDER TREATMENT AT TIME T,PIG 2,
1 * BODES'/'
RETURN
CONTINUE
REMOVE HIPIED TREATMENT EFFCIS FROM THE TREATMENT LIST.
CALL REROF(DUB, UCBER, UCBER, UCBER, UCBER, UCBER, UCBER, UCBER, UCBER, UCBER)
IF (UCBER.CT.0) GO TO 51
TBI = TIME / 3600.0
WRITE (80,210) TBI
RETURN
CONTINUE
DO LOOP OVER ALL TREATMENT EFFORTS.
DO 10 UCBER=1,UCBER
BC = UCBER(UCBER)
DETERMINE AREA WHICH MAY BE TREATED THIS TIME STEP.
TRAREA = (UCBER(UCBER) / UCBER(UCBER)) * (DT / 3600.0)
FIND ALL SPILLETS WITHIN RANGE OF TREATMENT EQUIPMENT.
CALL DIST(ASPIL(ISP), RSPIL(ISP), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER), UCBER(UCBER))
IF THE DISTANCE BETWEEN EFFORT AND SPILLET
IS TOO LARGE OR IF THE SPILLET HAS BEEN
COMPLETELY TREATED, THEN RETURN.
IF (DIS.CT.AC) RETURN
IF (ASPIL(ISP).LT.0.0) RETURN
IF A SPILLET IN THE AREA HAS BEEN PARTIALLY TREATED CONTINUE
TREATMENT.
IF (ASPIL(ISP).GT.0.0) GO TO 40
TREAT THIS SPILLET.
SPAREA = RSPIL(ISP)**2 * PI - ASPIL(ISP)
IF (TRAREA.LE.SPAREA) GO TO 40
RSPIL(ISP) = 1.0
ASPIL(ISP) = (-1.0) * RSPIL(ISP)**2 * PI

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Figure VII.-3. MAIN


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      BREAD = BSED / FLOAT(BRAD)
      WRITE(80,200) BREAD, TRZAB, BREAD
      WRITE(80,201) SIGI, SIGI, SIGI
200  FORMAT(' THE AVERAGE VALUES OF X, Y AND Z ARE',3F10.6)
201  FORMAT(' THE STANDARD DEVIATIONS ARE ',3E,3F10.6)
      CONTINUE
C
C
C
      B E T O B B B E E E
C
      IF( (DI.CY.O.O) .AND. (DT.CY.O.O) ) RETURN
C
      HERE FOR AN ERROR IN THE CALCULATION OF DI OR OF DT.
C
      WRITE(80,110) DI, DT
      FORMAT('O ERROR ',50(' ')/' DI=',E10.5,' DT=',E10.5)
110
C
C
      S T O P B E E E
C
      STOP
      END
      SUBROUTINE PARTV(IPP, VPP, UPP, EPP, TSP, EPP, B,
1  X, Y, Z, IP, JP, KP)
C
C
C
      SUBROUTINE DESCRIPTION
C
      THIS SUBROUTINE IS USED TO CALCULATE THE FLOW VELOCITY
      AT THE POSITION OF EACH OF THE BARREL PARTICLES. A LINEAR
      INTERPOLATION SCHEME IS USED FROM THE SUBROUTINE VELOCITY BODIES.
C
C
C
      .....
C
      COMMON STATEMENTS
      COMMON /PLOT/ BAIFA, BAIF1, BAIF2, AP, OFLT(15,15,10),
1  WPL(15,15,10), WPL1(15,15,10), EPL, EPL, EPL, EFS, EFS, EFS
      COMMON /CUTL/ JNSOB, JNSOB, RESUB, SPSTA,
1  SPSTC, DT, TIME, TIBRAB, ISCAL, USAV(200)
      COMMON /SDS/ STRABS, SUD, BEITS, BRAB, BRAB, DI, DT, DZ,
1  TORIC, TORIC, TORIC
C
C
C
      DIMENSION STATEMENTS
      DIMENSION I(BRAB), J(BRAB), K(BRAB)
      INTEGER B(15,15,10)
C
C
C
      S T A R T B E E E
C
      OBTAIN THE SUBSCRIPTS FOR THE GRID ELEMENT FOR THIS PARTICLE
      PI = IPP / DI
      IP = PI * 1
      PJ = TSP / DT
      JP = PJ * 1
      PK = IPP / DZ
      KP = PK * 1
C
C
      OBTAIN THE XYZ POSITION OF THE BARREL RELATIVE TO CELL CENTRE
      EP = PI - FLOAT(IP) * 0.5
      TP = PJ - FLOAT(JP) * 0.5
C
      SP = PK - FLOAT(KP) * 0.5
C
      OBTAIN THE XYZ POSITION OF THE PARTICLE RELATIVE TO CELL CORNER
      EQ = 0.5 + EP
      TO = 0.5 + TP
      SQ = 0.5 + SP
C
      MAKE SURE THAT NONE OF THE P SUBSCRIPTS ARE OUT OF RANGE
      IF(IP.GT.18500) IP=18500
      IF(IP.LT.1) IP=1
      IF(JP.GT.18500) JP=18500
      IF(JP.LT.1) JP=1
      IF(KP.GT.18500) KP=18500
      IF(KP.LT.1) KP=1
      IF( (IP, JP, KP) .EQ. (0,0,0) ) GO TO 16
      UPP=UPLT(IP, JP, KP)
      VPP=VPLT(IP, JP, KP)
      WPP=WPLT(IP, JP, KP)
      RETURN
16  CONTINUE
C
      OBTAIN SUBSCRIPTS OF CONTRIBUTING ELEMENTS TO THE VELOCITY AVG
      IF(IPP) 1, 2, 2
      IQ = IP - 1
      IIP = -IP
      GO TO 3
2  IQ = IP + 1
      IIP = IP
      IF(IPP) 4, 5, 5
      JQ = JP - 1
      ATP = -JP
      GO TO 6
5  JQ = JP + 1
      ATP = JP
      IF(IPP) 7, 8, 8
      IQ = IP - 1
      IIP = -IP
      GO TO 9
8  IQ = IP + 1
      IIP = IP
      RETURN
9  CONTINUE
C
      MAKE SURE THAT NONE OF THE Q SUBSCRIPTS ARE OUT OF RANGE
      IF(IQ.GT.18500) IQ=18500
      IF(IQ.LT.1) IQ=1
      IF(JQ.GT.18500) JQ=18500
      IF(JQ.LT.1) JQ=1
      IF(KQ.GT.18500) KQ=18500
      IF(KQ.LT.1) KQ=1
C
      CALCULATE THE U VELOCITY COMPONENT
      IX = IP - 1
      IF(IX.LE.0) IX = 1
      U1 = UPLT(IX, JP, KP)
      UY = UQ * ( UPLT(IP, JP, KP) - U1 ) * B1

```

```

      U2 = UPLT(IX, JP, KQ) - U2 ) * U2
      U3 = UPLT(IX, JQ, KP)
      U3 = UQ * ( UPLT(IP, JQ, KP) - U3 ) * U3
      U4 = UPLT(IX, JQ, KQ)
      U4 = UQ * ( UPLT(IP, JQ, KQ) - U4 ) * U4
      U31 = UPP * ( U3 - U1 ) * U1
      U32 = UPP * ( U4 - U2 ) * U2
      UPP = UPP * ( U32 - U31 ) * U31
C
      CALCULATE THE V VELOCITY COMPONENT
      JV = JP - 1
      IF(JV.LE.0) JV = 1
      V1 = VPLT(IP, JV, KP)
      V1 = UQ * ( VPLT(IP, JV, KP) - V1 ) * V1
      V2 = VPLT(IP, JV, KQ)
      V2 = UQ * ( VPLT(IP, JV, KQ) - V2 ) * V2
      V3 = VPLT(IQ, JV, KP)
      V3 = UQ * ( VPLT(IQ, JV, KP) - V3 ) * V3
      V4 = VPLT(IQ, JV, KQ)
      V4 = UQ * ( VPLT(IQ, JV, KQ) - V4 ) * V4
      V31 = UPP * ( V3 - V1 ) * V1
      V32 = UPP * ( V4 - V2 ) * V2
      UPP = UPP * ( V32 - V31 ) * V31
C
      CALCULATE THE Z VELOCITY COMPONENT
      EZ = KP - 1
      IF(EZ.LE.0) EZ = 1
C
      BE CAREFUL HERE! THE ADVECTIVE VELOCITY IN THE Z DIRECTION
      TO THE BOTTOM ELEMENT OF THE WATER COLUMN IS CALCULATED USING
      ONLY THE PLANT ABOVE THE ELEMENT AND NOT BY AVERAGING THE
      PLANT ABOVE AND THE PLANT BELOW AS IS IN ALL OTHER CASES
C
      U1 = UPLT(IP, JF, EA)
      U1 = UQ * ( UPLT(IP, JP, KP) - U1 ) * U1
      U2 = UPLT(IP, JQ, EA)
      U2 = UQ * ( UPLT(IP, JQ, KP) - U2 ) * U2
      U3 = UPLT(IQ, JF, EA)
      U3 = UQ * ( UPLT(IQ, JP, KP) - U3 ) * U3
      U4 = UPLT(IQ, JQ, EA)
      U4 = UQ * ( UPLT(IQ, JQ, KP) - U4 ) * U4
      U31 = UPP * ( U3 - U1 ) * U1
      U32 = UPP * ( U4 - U2 ) * U2
      UPP = UPP * ( U32 - U31 ) * U31
C
      B E T O B B B E E E
C
      RETURN
      END
      SUBROUTINE PRINT(C, B, X, Y, Z, BORDS, NST, DFLT, WPLT, CC)
C
C
C
      SUBROUTINE DESCRIPTION
C
      THIS SUBROUTINE HANDLES ALMOST ALL OUTPUT OPERATIONS.
C
C
C
      .....
C
      COMMON STATEMENTS
      COMMON /DEPOS/ BLOST, BDEP
      COMMON /DIFF/ BCRIT, BDIFF, BIL, DIT, DZ1, BIL, ETL
1  POSI, POSI
      COMMON /POTL/ BAIFA, BAIF1, AD, DEPTH(30,30), IDL, YDL,
1  IDS, YDS
      COMMON /SLVS/ SAKEX, SAKEX, AE, BCST(30,30), EEL, TEL,
1  EES, TES
      COMMON /PLOT/ BAIFA, BAIF1, BAIF2, AP, OFLT(15,15,10),
1  WPL(15,15,10), WPL1(15,15,10), EPL, EPL, EPL, EFS, EFS, EFS
      COMMON /CUTL/ JNSOB, JNSOB, RESUB, SPSTA,
1  SPSTC, DT, TIME, TIBRAB, ISCAL, USAV(200)
      COMMON /SDS/ STRABS, SUD, BEITS, BRAB, BRAB, DI, DT, DZ,
1  TORIC, TORIC, TORIC
      COMMON /PERT/ SPSTV, SPSTC, SPSTP, SPSTP, SPSTP, SPSTC, SPSTC,
1  SPSTP, SPSTP, SPSTP
      COMMON /PMTL/ BCLASS, BORDS(200), DDIAH(200), DDEE(200),
1  DBASS(200), DVELS(200), DCOSP(200, 8), BICLAS, BICL
      COMMON /SDS/ STRABS, SUD, BEITS, BRAB, BRAB, DI, DT, DZ,
1  TORIC, TORIC, TORIC
      COMMON /TIDE/ BAIT1, BAIT1, AT, OT(30,30), VT(30,30), ATLD, ITLD,
1  ITS, VTS, IEL, YEL
      COMMON /UNIT/ UNIT3(2)
C
C
C
      DIMENSION STATEMENTS
      DIMENSION C(15,15,10)
      DIMENSION DFLT(15,15), WPLT(15,15), CC(15,15)
      DIMENSION I(BRAB), J(BRAB), K(BRAB)
      DIMENSION BJO(30), BIO(30)
      DIMENSION WPLT(15,15,10), UPLT(15,15,10)
      INTEGER B(15,15,10)
      INTEGER*2 BORDS(BRAB)
C
C
C
      DATA STATEMENTS
C
      DATA B1 / 6 /
      S T A R T B E E E
C
      INITIALISE CALL FLAG SO AS NOT TO CALL COSC TWICE HERE.
      BCALL1 = 0
C
      FIX FORMAT STATEMENTS
C
      FIX DISTANCE FROM ORIGIN OF FIXED SYSTEM TO GRID LOCATIONS
      B11 = TORIC * IDS - 0.5*DI
      U1 = TORIC * IDS - 0.5*DI
      DO 150 I=1, 18500
      B11 = B11 + DI
      BIO(I) = B11
      DO 160 J=1, 18500
      U1 = U1 + DT
      B11 = U1 + DT
150  B11 = U1
160
C

```

Figure VII.-3. MAIN


```

C
C
C      S T A R T   M E N U
C
C      BEGIN PSEUDO TOTAL VELOCITIES.
C
C      DO 5 I=1, IBSUB
C      DO 5 J=1, JSUBI
C      DO 5 K=1, KSUBI
C      VPLT(I, J, K)=0.0
C      VPLT(I, J, K)=0.0
C      VPLT(I, J, K)=0.0
C
C      BEGIN REAL VELOCITY VARIABLES USED IN THE COUPLER CALCULATION
C
C      UBAR1 = 0.0
C      VBAR1 = 0.0
C      WBAR1 = 0.0
C      UBAR2 = 0.0
C      VBAR2 = 0.0
C      WBAR2 = 0.0
C
C      INTERPOLATE ADVECTIVE VELOCITY FIELD FROM PSEUDOHYDRAVIC FIELD
C
C      IF (STARS.EQ.0) CALL VPLT ( VPLT, VPLT )
C
C      CALCULATE SCALE DEPENDENT DIFFUSION COEFFICIENTS
C
C      DISC=0.0
C      DISC=0.0
C      IF (DISC.EQ.1) CALL DISP ( I, J, K )
C
C      INITIALIZE VARIABLES TO BE USED IN DIFFUSIVE VELOCITY CALC
C
C      DEF = DZ1 * (-2.0)
C      ARS00 = FLOAT ( ARS00 )
C      JRS001 = JRS00 - 1
C      JRS002 = JRS00 + 1
C      KRS001 = KRS00 - 1
C      KRS002 = KRS00 + 1
C
C      DO LOOP OVER GRID ELEMENTS
C
C      DO 1 I=1, IBSUB1
C
C      FIND LATITUDE IF NEEDED TO CONVERT DEGREES TO METERS
C
C      TO = (TOSIG*FDS)+YDL-DY
C
C      DET AND DT: ARE TO BE IN METERS ALWAYS, DE ARE DT*DC*SC
C
C      DO 1 J=1, JSUB1
C      DT = DE
C      IF (ISCAL.EQ.1) GO TO 45
C      TO = TO + DE
C      SCAL = 6371.0*1000.0*3.6*1000/100.0
C      DT = DT*SCAL
C      DET = DE*SCAL*205(50/57.296)
C      NOW THESE ARE IN METERS.
C 45 CONTINUE
C
C      STORE ARRAY ELEMENTS TO BE USED RECURSIVELY BELOW
C
C      RIJ = VPLT ( I, J )
C      RIJ1 = VPLT ( I-1, J )
C      RIJ2 = VPLT ( I+1, J )
C      RIJ3 = VPLT ( I, J-1 )
C      RIJ4 = VPLT ( I, J+1 )
C      RIJ5 = VPLT ( I-1, J-1 )
C      RIJ6 = VPLT ( I-1, J+1 )
C      RIJ7 = VPLT ( I+1, J-1 )
C      RIJ8 = VPLT ( I+1, J+1 )
C      RS = RIJ + RIJ1
C      DO 1 K=1, KSUB1
C
C      SKIP THIS GRID ELEMENT IF IT IS NOT A COMPUTATIONAL CELL
C
C      IF (R(I, J, K).EQ.0) GO TO 1
C
C      CALCULATE THE DIFFUSION COEFFICIENT TIES: (-2) / DT
C
C      DIQ = -2.0/DET
C      DIJ = -2.0/DET
C      DIP = DZ1 + DIQ
C      DIP = DZ1 + DIJ
C
C      BEGIN THE DIFFUSION VELOCITY
C
C      UD = 0.0
C      VD = 0.0
C      WD = 0.0
C
C      FIND THE BASIS VELOCITY/GRID VALUE FOR THE COUPLER CALCULATION
C
C      IF (ABS ( VPLT ( I, J, K ) / DT ) .GT. DBAR1)
C 1 UD = ABS ( VPLT ( I, J, K ) / DT )
C      IF (ABS ( VPLT ( I, J, K ) / DT ) .GT. VBAR1)
C 1 VBAR1 = ABS ( VPLT ( I, J, K ) / DT )
C      IF (ABS ( VPLT ( I, J, K ) / DT ) .GT. WBAR1)
C 1 WBAR1 = ABS ( VPLT ( I, J, K ) / DT )
C
C      SKIP CALCULATION OF DIFFUSION VELOCITY IF LESS THAN A CRITICAL
C      NUMBER OF PARTICLES HAVE BEEN STRAIGHTENED.
C
C      IF (DBAR1.LT.UBAR1) GO TO 12
C
C      IF ANALYTICAL DIFFUSION IS TO BE USED SKIP NEXT PORTION
C
C      IF (PARR.EQ.1) GO TO 12
C
C      STORE CONCENTRATION VALUES AND CHECK FOR CONCENTRATION = 0
C
C      C1J = C ( I, J, K )
C      C1J1 = C ( I-1, J, K )
C      C1J2 = C ( I+1, J, K )
C      C1J3 = C ( I, J-1, K )
C      C1J4 = C ( I, J+1, K )
C      C1J5 = C ( I-1, J-1, K )
C      C1J6 = C ( I-1, J+1, K )
C      C1J7 = C ( I+1, J-1, K )
C      C1J8 = C ( I+1, J+1, K )
C      CDIP1 = C1J1 - C1J2
C      CDIP2 = C1J3 - C1J4
C      CDIP3 = C1J5 - C1J6
C      CDIP4 = C1J7 - C1J8
C      CDIP5 = C1J1 - C1J3
C      CDIP6 = C1J2 - C1J4
C      CDIP7 = C1J5 - C1J7
C      CDIP8 = C1J6 - C1J8
C      SE = FLOAT ( SE )

```

Figure VII.-3. MAIN


```

//Z189418 JOB (Z1100), 'DATAOUT', BSLEVEL=1
//* EXEC SCDS9,DS9=BSL, Z11,DEBDC,PBREV:V
//* EXEC DSALOC
//*MSHARE1 DD DS9=BSL, Z11,DEBDC,PBREV,DISP=(BEU,CATLG),
//* UNIT=SYSDA,SPACE=(TRK,(5,1),RLSE),
//* DCB=(RECFM=FBS,BLKSIZE=1954)
// EXEC FORMCON,REGION=GO=927,P1='SYSOUT=(C,,2019)',
// '93''SYSOUT=(C,,2019)'
//PART.SISIP DD *
C
C      PROGRAM DESCRIPTION
C
C      THIS PROGRAM READS THOSE DATA OUTPUT BY OILSP AND
C      AND PRINTS THIS DATA OUT ON PAPER OR IN A REDUCED FORM TO DISK.
C
C      VARIABLE DESCRIPTION
C
C      BPPT CONTROLS THE PRINTOUT.
C
C      - 1 PRINT OUT TO DISK FOR PLOTTING ROUTINES
C      - 0 NO PRINTOUT
C      - 1 PRINT ONLY AS FEED IF
C      - 2 PRINT ONLY FORMATTED OUTPUT
C      - 3 PRINT BOTH AS FEED IF AND FORMATTED OUTPUT.
C
C      BRDPT CONTROLS READING OF PARTICLE DATA SET
C
C      - 0 PARTICLES NOT FEED
C      - 1 PARTICLES FEED IN THAT UNIT
C
C      CCUT - THIS IS THE BIRTH* CONCENTRATION IN
C      PARTS PER THOUSAND WHICH IS TO BE USED
C      FOR OUTPUT.
C
C      BRDCR CONTROLS READING OF THE CONCENTRATION DATA SET
C
C      BRDSP CONTROLS READING OF THE SPILLER DATA SET
C
C-----
C      DIMENSION STATEMENTS
C
C      DIMENSION DSPIL(11), DSPIL(11), PSPIL(61), SSPIL(61),
C      DSPIL(61), MSPIL(61), TSPIL(11), USPIL(11), CSPIL(61,8)
C      DIMENSION NUNBD(100), DCON(100,8), DDIR(100), DDIR(100),
C      DRASS(100), DVEL(100)
C      DIMENSION I(2000), J(2000), K(2000), L(2000)
C      DIMENSION CT(899), IC(899), JG(899)
C      INTEGER*2 NUNBD(2000)
C
C      DATA STATEMENTS
C
C      DATA NUN, PI / 6, 3.14159/
C
C      S T A T I S T I C S
C
C      WRITE(NN,445)
C 445 FORMAT('1 INPUT PARAMETERS')

```

```

IF (BPPT.EQ.-1) PRINT 7, DAY, TIME, NSPIL
FORMAT(2I,10,3I,F15.5,3I,110)
DO 100 I=1,NSPIL
IF (I.CT.) READ (NPOST) TIME, NSPIL
READ (NPOST,END=901) I1, DSPIL(I), DSPIL(I), TSPIL(I), MSPIL(I),
1 DSPIL(I), DSPIL(I), SSPIL(I), USPIL(I), CSPIL(I), J1, J1, E)
IF (NPOST.EQ.1) OR (BPPT.EQ.3)
1 WRITE (NUN,20) I1, DSPIL(I), TSPIL(I), MSPIL(I),
1 DSPIL(I), DSPIL(I), SSPIL(I), USPIL(I), CSPIL(I), J1, J1, E)
FORMAT(2I,13,8F10.3/5I,8F8.2/)
C
C      CONVERT GR/CC TO TONS/R**3
C
C      DEN = DSPIL(I) * 0.5
C
C      DETERMINE THE VOLUME OF THE SLICK AND THEN
C      THE SPILLER THICKNESS.
C
C      VOL = DSPIL(I)/DSPIL(I)
C      THIC = VOL/(PI*DSPIL(I)*PSPIL(I))
C      IF (BPPT.EQ.-1) WRITE (2) TSPIL(I), MSPIL(I), USPIL(I), TSPIL(I)
100 CONTINUE
GO TO 951
C
C      HERE IF AN EOF WAS ENCOUNTERED ON UNIT 1
C
C 901 CONTINUE
PRINT 801
801 FORMAT('0',50('**'), ' EOF ENCOUNTERED ON UNIT 1'/)
STOP
951 CONTINUE
IF (BRDCE.EQ.0) GO TO 1
C
C      READ IN CONCENTRATION PARAMETERS
C
C      READ (BRDCR,END=910) IMSDB, JMSDB, PMSUP, NRAI, WCLASS, WFLG, RCT, RCT,
1 RDEF, CT, PL, IC, CG, YC, YG, YC, YG, YC, YG, YC, YG, YC, YG, YC, YG, YC, YG,
1 IF (RDEF.EQ.1) OR (RDEF.EQ.2)
1 WRITE (NUN,10) PMSUP, PMSUP, PMSUP, PMSUP, PMSUP, PMSUP, PMSUP, PMSUP,
1 TIME, TIME, TIME, TIME, TIME, TIME, TIME, TIME, TIME, TIME, TIME, TIME,
10 FORMAT(2I,9I,3I,F15.3,8F10.3,5F10.6)
READ (BRDCR,END=910) (IC(I), I=1, 899)
READ (BRDCR,END=910) (JG(I), I=1, 899)
IF (RDEF.EQ.1) OR (RDEF.EQ.2)
1 WRITE (NUN,24) (IC(I), I=1, 899)
1 IF (RDEF.EQ.3) OR (RDEF.EQ.3)
1 WRITE (NUN,24) (JG(I), I=1, 899)
FORMAT(2I,15F6.3/)
24 DO 95 P=1, 899
READ (BRDCR,END=910) (CONC(I, J, K, L), I=1, 899)
IF (CONC(I, J, K, L).EQ.0) OR (CONC(I, J, K, L).EQ.1)
1 WRITE (NUN,95) (CONC(I, J, K, L), I=1, 899)
FORMAT(5I,15F8.2)
95 CONTINUE
GO TO 960
C
C      HERE IF AN EOF WAS ENCOUNTERED ON UNIT 10.
C
C 910 CONTINUE
PRINT 810
810 FORMAT('0',50('**'), ' EOF ENCOUNTERED ON UNIT 10'/)
STOP
960 CONTINUE
C
C      AVERAGE CONCENTRATION OVER WATER COLUMN FEED RATE AND DISK 1 AND 1
C      AND OUTPUT TO DISK IF REQUESTED.
C
C      NRAI = 0.0
C      TRAI = 0.0
C      TRIP = FLOAT(JMSDB) * D1
C      TRIP = FLOAT(JMSDB) * D1
C      IGRD = -D1
C      SUR = 0.0
C      RSUR = 0
C      DO 400 J=1, JMSUP
C      IGRD = IGRD * D1
C      IGRD = -D1
C      DO 400 J=1, JMSUP
C      CC(I, J) = IGRD * D1
C      DO 410 K=1, RNSUB
C      CC(I, J) = CC(I, J) + CONC(I, J, K)
C 410 CONTINUE
C      CC(I, J) = CC(I, J) * 1000.0 / FLOAT(RNSUB)
C      IF (CC(I, J).LT. CCUT) GO TO 400
C      SUR = SUR + D1 * D1
C      RSUR = RSUR + 1
C      CT(RNSUB) = CC(I, J) * 1000.0
C      IGRD = IGRD * IGRD
C      IGRD = IGRD * IGRD
C      IF (IGRD.EQ.1) TRAI = IGRD
C      IF (IGRD.EQ.2) TRAI = IGRD
C      IF (IGRD.EQ.3) TRAI = IGRD
C 400 CONTINUE
SUR = SUR / (50. * 50.)
C
C      CONVERT TO LONGITUDE AND LATITUDE.
C
C      NRAI = NRAI * XDS = (NORIG - 1.0) * D1 / 2.0
C      TRAI = TRAI * YDS = (YORIG - 1.0) * D1 / 2.0
C      TRAI = TRAI * YDS = (YORIG - 1.0) * D1 / 2.0
C      TRAI = TRAI * YDS = (YORIG - 1.0) * D1 / 2.0
C      IF (AD.WL.C.O) GO TO 67
C      IF (SCALE.EQ.2) GO TO 65
C      TRAI = TRAI * (YRAI - TRAI) / (2.0 * SCALE)
C      TRAI = TRAI * SCALE
C      NRAI = NRAI / (SCALE * COS (TRAI / 57.296))
C      TRAI = TRAI / (SCALE * COS (TRAI / 57.296))
C 65 NRAI = NRAI - TRAI
C      TRAI = TRAI - TRAI
C      TRAI = TRAI - TRAI
C 67 CONTINUE
C      DO 609 K=1, RNSUB
C      IGRD(K) = IGRD(K) * 100 * (10010 - 1.0) * D1 / 2.0
C      IGRD(K) = IGRD(K) * 100 * (10010 - 1.0) * D1 / 2.0
C      IF (AD.WL.C.O) GO TO 609
C      IF (SCALE.EQ.2) GO TO 77

```

Figure VII.-4. DATAOUT

```

77      YG(KR) = YG(KP)/SCALE
        YLAT = YDL*YG(KA)
        YG(KR) = YG(KP)/(SCALE*COS(YLAT/57.296))
        CONTINUE
609     YG(KR) = YDL*YG(KP)
        CONTINUE
        DIT = DI
        DTI = DI
        IF (ISCAL.EQ.1) GO TO 96
        YLAT = (YRAI*YDIR)/2.0
        DIT = DI*SCALE
        DTI = DI*SCALE*COS(YLAT/57.296)
96     CONTINUE
        IF (NPT.EQ.-1) PRINT 2, XDIR, YDIR, ZDIR, XDIR, YDIR, ZDIR, AD, XDIR, YDIR, ZDIR
        IF (NPT.EQ.-1) GO TO 465
        WRITE(2) XDIR, YDIR, ZDIR, XDIR, YDIR, ZDIR, AD, XDIR, YDIR, ZDIR
        DO 55A I=1, NPT
          WRITE(2) I, XDIR(I), YDIR(I), ZDIR(I)
55A     CONTINUE
665     CONTINUE
C
C     READ IN PARTICLE PARAMETERS
C
        IF (NPT.EQ.0) GO TO 1
        READ (NPT, 240-244) I, J, K, L, M, N, O, P, Q, R, S, T, U, V, W, X, Y, Z
        IF (NPT.EQ.1) .OR. (NPT.EQ.3)
          1 WRITE (NPT, 245) I, J, K, L, M, N, O, P, Q, R, S, T, U, V, W, X, Y, Z
        READ (NPT, 246-248) X1, Y1, Z1, X2, Y2, Z2, X3, Y3, Z3
        XDIR = (X1+X2+X3)/3.0
        YDIR = (Y1+Y2+Y3)/3.0
        ZDIR = (Z1+Z2+Z3)/3.0
        IF (NPT.EQ.1) .OR. (NPT.EQ.3)
          1 WRITE (NPT, 249) XDIR, YDIR, ZDIR
        IF (NPT.EQ.1) .OR. (NPT.EQ.3)
          1 WRITE (NPT, 250) XDIR, YDIR, ZDIR
        DO 66C I=1, NPT
          1 READ (NPT, 251-255) R, XDIR(I), YDIR(I), ZDIR(I), DR, DTHICK(I), DRASS(I)
          1 WRITE (I, 256) DR, XDIR(I), YDIR(I), ZDIR(I)
          1 IF (NPT.EQ.1) .OR. (NPT.EQ.3)
            1 WRITE (NPT, 257) DR, XDIR(I), YDIR(I), ZDIR(I)
          1 IF (NPT.EQ.1) .OR. (NPT.EQ.3)
            1 WRITE (NPT, 258) DR, XDIR(I), YDIR(I), ZDIR(I)
          1 IF (NPT.EQ.1) .OR. (NPT.EQ.3)
            1 WRITE (NPT, 259) DR, XDIR(I), YDIR(I), ZDIR(I)
66C     CONTINUE
C
C     READ IN PARTICLE POSITIONS
C
        DO 66 R=1, NPT
          READ (NPT, 260-264) XDIR(R), YDIR(R), ZDIR(R), XDIR, YDIR, ZDIR
          XDIR = XDIR + XDIR*DR
          YDIR = YDIR + YDIR*DR
          ZDIR = ZDIR + ZDIR*DR
          IF (NPT.EQ.1) .OR. (NPT.EQ.3)
            1 WRITE (NPT, 265) XDIR, YDIR, ZDIR
66     CONTINUE
66     PRINT (NPT, 266) XDIR, YDIR, ZDIR
        GO TO 961
C
C     HERE IF AN EOF WAS ENCOUNTERED BY THE END OF THIS
C
661     PRINT IF AN EOF WAS ENCOUNTERED BY THE END OF THIS
C
911     CONTINUE
        PRINT 811
661     POPRAT('0',50(' ',' '), ' EOF ENCOUNTERED ON DR: 11')
961     CONTINUE
        IF (NPT.LT.2) GO TO 1
C
C     HERE FOR FORMATTED PRINT OUT
C
        PRINT OUT HEADER FOR SPILLET INFORMATION.
C
        WRITE (NPT, 200) TIME
        POPRAT('1', 229, 'LISTING SPILLETS ', 'P. 3, ' HOOPS AFTER'
          1 ' THE BEGINNING OF THE SPILL', '11', '229, 65(' ',' '), '
          IF (NPT.LT.0) GO TO 300
        WRITE (NPT, 210)
        POPRAT('301', 'SPILLETS CREATED PRIOR TO THIS STEP')
C
C     DO LOOP OVER ALL EXISTING SPILLETS.
C
        DO 11 I=1, NPT
          IF (I-NSPIL-1) 26, 21, 26
C
C     HERE TO PRINT OUT HEADER FOR SPILLETS.
C
        21     CONTINUE
          WRITE (NPT, 220)
          POPRAT('0', 301, 'NEW SPILLETS ADDED THIS STEP')
        26     CONTINUE
C
C     PRINT OUT ALL SPILLET PARAMETERS.
C
        1     WRITE (NPT, 230) I, NSPIL(I), NSPIL(I), NSPIL(I), NSPIL(I)
        230    POPRAT(41, 'THE', '11', ' SPILLET APPEARED ', 'P. 2,
          1 ' HOOPS AFTER THE BEGINNING OF THE SPILL', '11', '11', '
          2 ' CENTERED AT LONGITUDE ', 'F10.6, ' AND LATITUDE ', 'F10.6,
          3 ' RADIUS OF SPILL ', 'F10.2,
          4 ' MASS AND IS OF WEIGHT ', 'F10.4, ' RESIDUAL TONN.'
        240    WRITE (NPT, 240) NSPIL(I), NSPIL(I), NSPIL(I)
          POPRAT(41, 'MORE PROPERTIES OF THE SPILLET ARE:')
          1 201, ' DENSITY ', '121, F10.6, ' GRAMS/CC/201,
          2 ' INTERFACIAL TENSION ', 'F10.6, ' DYNES/CM/201,
          3 ' KINEMATIC VISCOSITY ', 'F10.6, ' CENTISTOKES')
        250    WRITE (NPT, 250) (NSPIL(I), J=1, 8)
          POPRAT(41, 'BY WEIGHT THE OIL FRACTIONS ARE:')
          1 'PARAFFIN (C6-C12)', '101, F10.6/561,
          2 'PARAFFIN (C13-C22)', '91, F10.6/561,
          3 'CYCLOPARAFFIN (C6-C12)', '51, F10.6/561,
          4 'CYCLOPARAFFIN (C13-C22)', '41, F10.6/561,
          5 'AROMATIC (C6-C11)', '101, F10.6/561, 'AROMATIC (C12-C18)',
          6 '91, F10.6/561, 'AROMATIC-AROMATIC (C9-C25)',
          7 '11, F10.6/561, 'RESIDUAL', '191, F10.6)
        11     CONTINUE
        300     CONTINUE
C
C     PRINT 3-D CONCENTRATION FIELD AT EACH Z-LEVEL
C
        PRINT 102
        POPRAT('11')
        DO 10 R=1, NPT

```

Figure VII.-4. DATAOUT

```

//E2305678 JOB (E21100,100,2,5,,2019),'CHECDATA',MSGLEVEL=1
// EXEC PGM=CC,REGION,GO=1000,P1=STROUT(C,2019)
// P3=STROUT(C,2019)
//PORT.SYSIB DD *
C
C          PROGRAM DESCRIPTION
C
C THIS PROGRAM READS IN THE OUTPUT GENERATED BY THE PROGRAM DATAOUT
C AND PRINTS THIS DATA OUT.
C
C      UNIT - UNIT FROM WHICH THIS DATA IS READ FROM
C
C      NBDCH - CONTROLS WHETHER CONCENTRATION PARAMETERS
C             ARE READ IN
C             - 0 PARAMETERS NOT READ IN.
C             - 1 PARAMETERS ARE READ IN.
C
C          VARIABLE DESCRIPTIONS
C
C-----
C          DIMENSION STATEMENTS
C
C          DIMENSION RSPIL(30), YSPIL(30), RSPIL(30)
C          DIMENSION IC(899), YC(899), CT(899)
C
C          DATA STATEMENTS
C
C          DATA W0, P1/ 6, 3.14159/
C
C          WRITE(88,447)
C 447  FORMAT('1' INPUT PARAMETERS)
C
C          S T A R T   H E R E
C
C          READ IN CONTROL PARAMETERS.
C
C          CALL READI (RUNIT, 'RUNIT ', 0, 15)
C          CALL READI (NBDCH, 'NBDCH ', 0, 1)
C
C          REFER TO IT E P A C E O V E R   T I P E   S C I T E
C
C          PRINT 5
C          FORMAT('1')
C          CONTINUE
C
C          READ IN JULIAN DAY AND NUMBER OF SPILLS.
C
C          READ (RUNIT,RD=901) IDAYS, TIME, RSPIL
C          PRINT 10, IDAYS, TIME
C 10   FORMAT('///101,SPILLET PARAMETERS FOR JULIAN DAY',IS,
C            ' BEICH IS',P15.5,' RODS FROM THE START OF THE SPILL'
C            //2, /20, 'SPILLET LOCATIONS AND FACI//50,
C            ' SPILLET 0, 121, 'LONGITUDE', 121, 'LATITUDE', 121, 'RADIUS',
C            121, ' THICKNESS')
C          DO 100 I=1, RSPIL
C            READ (RUNIT, RD=901) RSPIL(I), YSPIL(I), RSPIL(I), THIC
C            PRINT 30, I, RSPIL(I), YSPIL(I), RSPIL(I), THIC
C 20   FORMAT(51.15, 101.0 (F15.5, 51))
C
C
C 100  CONTINUE
C       IF(NBDCH.EQ.0) GO TO 1
C
C          READ IN SUBSURFACE PARTICLE LIMITS
C
C          READ (RUNIT, RD=901) R1R, IDAL, TRIP, TRAL, DL, DL, RSDR, AC, RDL, YDL
C          WRITE(88, 32) DL, DL, RSDR
C 32   FORMAT(21, 'THE GRID SEPARATION IN THE X DIRECTION IS', P10.2,
C            ' METERS', 'AND IN THE Y DIRECTION IS', P10.2, ' METERS',
C            2 ' AND THERE ARE ', I4, ' GRIDS OVER THE RIBBON CONCENTRATION')
C
C          CONVERT TO DEGREES FOR PRINTOUT
C
C          AD = AD * 57.296
C          WRITE(88, 69) AD, YDL, YDL
C 69   FORMAT(21, '51, 'THE DEPTH GRID HAS BEEN ROTATED ', P6.4,
C            ' IN THE COURSE CLOCKWISE DIRECTION', //42,
C            2 ' AND HAS AN OFFSET OF ', P7.3, ' M', P7.3, ' M')
C          WRITE(88, 33)
C 33   FORMAT(//52, 'LONGITUDE', 11, 'LATITUDE', 11, 'PARTS/BILLION')
C          DO 700 R=1, RSDR
C            READ(RUNIT) IC(RR), YC(RR), CT(RR)
C            WRITE(88, 710) IC(RR), YC(RR), CT(RR)
C 710   FORMAT(31.2F10.8, 11, F11.2)
C 700  CONTINUE
C          PRINT 30, IDAL, TRIP, TRAL, THIC
C 30   FORMAT('ORAL: SUN LONGITUDE', P15.5/ ' RIBBON LONGITUDE', P15.5/
C            ' RIBBON LATITUDE', P16.5/ ' RIBBON LATITUDE', P16.5)
C          GO TO 1
C
C          HERE IF AN EOF WAS ENCOUNTERED OF UNIT 1
C
C 901  CONTINUE
C       PRINT 801
C 801  FORMAT('0', 50('**'), ' EOF ENCOUNTERED OF UNIT 1//)
C 951  CONTINUE
C       STOP
C       END
C       SUBROUTINE READI (C, ICHAR, NL, ND)
C       REAL*8 ICHAR, ICHARI
C       DATA N0, N0/5, 6/
C       READ (88, 10) I, ICHARI
C 10   FORMAT(15, 51, A8)
C       IF(ICHARI.EQ. ICHAR) GO TO 100
C       WRITE (88, 70) ICHARI, ICHARI
C 70   FORMAT(21H CARDS OUT OF ORDER ,A8, 66 READ ,A6, 10F REQUESTED)
C       STOP
C 100  CONTINUE
C       IF(EL.EQ. ND) GO TO 200
C       IF( (I.GE. NL) .AND. (I.LE. ND) ) GO TO 200
C       WRITE (88, 80) ICHAR, NL, ND, ICHARI, I
C 80   FORMAT(14H0 THE LIMITS OF ,A8, 58 ARE ,15, 4E TO ,15,
C            1 ' 68, BUT ,A6, 16' WAS READ IN AS ,15)
C       STOP
C 200  CONTINUE
C       WRITE (88, 30) I, ICHARI
C 30   FORMAT(21, 15, 51, A6)
C       RETURN
C       END
//NO.SYSIB DD *

```

```

1  UNIT
0  UNIT
//NO.PY01001 DD DSN=VAL.E211.D2306.P01V01,DISP=OLD
//

```

Figure VII.-5. CHECDATA


```

DO 121 I=1,NSC
121 TRASS(I)=TRASS(I)+XNATS(I)
IF (A.EQ.1) CALL L191(TIME,TRASS,NSC,1,0,0)
IF (A.EQ.2) CALL DASH(TIME,TRASS,NSC,1)
YT = TRASS(NSC)/TRASS(NT)
DIP = TO - YT
IF (ABS(DIP).LE.0.16) YT = YT - 0.165
CALL STBOL(BLAS,YT,.16,'0',0,0,1)
TO = YT
Y1 = Y1-0.16
WRITE(SV,547)
547 FORMAT(21,' MASS IS ATMOSPHERE PLOTTED')
CALL STBOL(B1,Y1,.16,'0 - MASS IS ATMOSPHERAL',
1 0,0,23)
C
C PLOT TOTAL AMOUNT OF MASS DUMPED
C
109 IF (NDSP.EQ.0) GO TO 129
IF (A.EQ.1) CALL L191(TIME,NDSP,NSC,1,0,0)
IF (A.EQ.2) CALL DASH(TIME,TRASS,NSC,1)
YT = NDSP(NSC)/NDSP(NT)
DIP = TO - YT
IF (ABS(DIP).LE.0.16) YT = YT - 0.165
CALL STBOL(BLST,YT,.16,'0',0,0,1)
TO = YT
Y1 = Y1-0.16
WRITE(SV,548)
548 FORMAT(21,' TOTAL MASS SPILLED PLOTTED')
CALL STBOL(B1,Y1,.16,'0 - TOTAL MASS SPILLED',
1 0,0,23)
129 CONTINUE
IF (NPLOT.EQ.1) CALL PLOT(0,0,0,0,3)
C
C IF SVS = RESO, THEN USE THE SAME DATA
C TO DO ANOTHER PLOT.
C
IF (SVS.EQ.0) Y1 = 0.75
IF (SVS.EQ.0) GO TO 77
CONTINUE
CALL PLOT(0,0,0,0,999)
RETURN
END
SUBROUTINE READI(I,ISABE,BL,SU)
REAL*8 ISABE, IPRABE
DATA NS,NS/5,6/
READ (IS,10) I,IPRABE
10 FORMAT (I15,SI,4E)
IF (IPRABE.EQ.ISABE) GO TO 100
WRITE (SV,20) IPRABE, ISABE
20 FORMAT (21M CARDS OUT OF ORDER ,AS,6E READ ,AB,10E BL,US,1E)
STOP
100 CONTINUE
IF (BL.EQ.SU) GO TO 200
IF (I.GE.BL) .AND. (I.LE.SU) GO TO 200
WRITE (SV,40) ISABE, BL, SU, ISABL, I
40 FORMAT (16M THE LIMITS OF ,AB,5E ARE ,IS,6E TO ,IS,
1 6E. NOT ,AS,16E HAS READ IN AS ,IS)
STOP
200 CONTINUE
WRITE (SV,30) I, ISABE
30 FORMAT (21,I15,SI,4E)

```

Figure VII.-6. PLOTMASS

```

//K230678 JOB (BIA100), 'PLOT AREA EXTENT'
//* EXEC SCRD05,DSN=001.EIAT.AREA
//* EXEC DSAL00
//* DD DSN=001.EIAT.AREA,SPACE=(TRM,(4,2)),
//* UNIT=SYSDA,DISP=(,CATLG),
//* DCB=(RECFM=FBS,BLSIZE=1554)
// EXEC POSTGCC,REGION GO=12M,LIB=CPL01,
// P1=SYSDUT=(C,,2019),P3=SYSGUT=(C,,2019)
//POST.SIZES DD =
C
C THIS PLOTTING PROGRAM CALCULATES AND PLOTS THE
C AREA EXTENT OF THE SUBFACE SPILLETS AND SUBSUBFACE
C GRID OVER A THRESHOLD LEVEL AS DETERMINED BY THE PROGRAM CRITERIA.
C IT ONLY INCLUDES THE SPILLETS WHICH ARE THICKER
C THAN THE INDICATED MINIMUM
C THIS PROGRAM READS THE UNIT NUMBER IN THE LOOP AS
C DEFINED THE VARIABLE J4. IF ONLY ONE PLOT IS BEING
C DONE, THE UNIT NUMBER IS THEREFORE 1 THE CASE WHICH
C HAS THE HIGHER EXTENT ALWAYS HAS TO HAVE ITS DATA SET AS
C UNIT ONE AS THE SCALE FACTOR IS DETERMINED BY USING THE
C DATA FROM THAT UNIT OTHERWISE SOME DATA MAY BE PLOTTED
C OFF OF THE PAPER.
C THE VARIABLE SAS CONTROLS WHETHER THE SUBSUBFACE,
C SURFACE, OR BOTH ARE TO BE PLOTTED.
C SAS = -1 - PLOT SUBFACE ONLY
C       0 - PLOT SUBSURFACE ONLY
C       1 - PLOT BOTH
C
C-----
C      DIMENSION XSPIL(20), YSPIL(20), ASPIL(20),
C      TISE(100), CONC(200)
C      DIMENSION ASUB(50), ATOT(50), ATOTP(50)
C      DATA PI, BU, J, I, I59, 6
C      WRITE(88,887)
C887  FORMAT('1'  I59T PARANTHESES')
C
C READ NUMBER OF STEPS AND LENGTH OF TIME STEPS IN SECONDS
C
C      CALL READI( SAS, 'SAS', 1, 1)
C      CALL READI( SPLOT, 'SPLOT', 1, 5)
C      CALL READI( THICK, 'THICK', 1)
C      CALL READI( NSTEP, 'NSTEP', 0, 100)
C      CALL PLOTS(0,0,6)
C
C DO LOOP OVER THE DATA SETS
C
C      DO 200 J4=1,SPLOT
C      BL = 0
C      WRITE(88,885) J4
C885  FORMAT('1', ' NOW PLOTTING CASE ', I4)
C      IF (J4.EQ.5) J4 = 10
C      DO 20 I=1,NSTEP
C      ATOT(I)=0.0
C      ASUB(I) = 0.0
C      ATOTP(I) = 0.0
C      ASUBP(I) = 0.0
C20  ASUBP(I) = 0.0
C
C ITERATE OVER STEPS
C
C      DO 100 SB=1,NSTEP
C10  READ(J4) IDAT, TISE(SB), XSPIL
C
C      ASP = 0.0
C
C LOOP OVER THE SPILLETS AND CALCULATE THE AREA OF EACH
C
C      DO 3 I=1,NSPIL
C      READ(J4,END=100) XSPIL(I),YSPIL(I),NSPIL(I), THIC
C
C IF SPILLET IS NOT THICK ENOUGH, DO NOT INCLUDE IT
C
C      IF (THIC.LT THICK) GO TO 3
C      ASP = XSPIL(I)/1000.0
C      ASPT = YSPIL(I)/NSPIL(I)
C      ASP=ASP*ASPT
C3  CONTINUE
C      ASUB(SB) = ASP
C      SUBCLS = 0
C      IF (SAS.EQ.-1) GO TO 29
C      READ(J4,END=100) XCOLS, XCOLR, YCOLS, YCOLR, DR, DT, SWELL, AL, ALL, PL
C
C READ IN ELEMENTS POSITION AND CONCENTRATION
C
C      DO 5 I=1,NURLES
C      READ(J4,END=100) EG, YG, CG
C5  CONTINUE
C      DI = DI/1000.0
C      DT = DT/1000.0
C      ASUB(SB) = SUBCLS*DI*DT
C29  CONTINUE
C      WRITE(88,827) XURLES, YSPIL, TISE(SB)
C827  FORMAT('1', ' XURLES ARE', I4, ' CONCENTRATION VALUES ARE',
C      1 I4, ' SPILLETS OUT TAKE AT TIME ', F12.2, ' HOURS')
C      ATOT(SB) = ASUB(SB) + ASUB(SB)
C      WRITE(88,28) ASUB(SB), ASUB(SB), ATOT(SB)
C28  FORMAT('101,F12.4, ' SQUARE KILOBYTES OF SUBFACE',
C      1 ' 101,F12.4, ' SQUARE KILOBYTES IN SUBSUBFACE',
C      2 ' 101,F12.4, ' TOTAL AREA EXTENT',)
C100  CONTINUE
C      ST = NSTEP-2
C      IF (J4.EQ.1) GO TO 67
C
C NOW LETS DO SOME PLOTTING
C
C      CALL RECT(0.75,0.75,10 0,7.75,0.0,3)
C      CALL SYMBOL(0.0,0.75,0.25, ' AREA COVERED BY SPILL',0,0,22)
C      X1 = 0.5
C      Y1 = 9.10
C      CALL SCALE(TISE,6.0,NSTEP,1)
C      IF (SAS.EQ.1) CALL SCALE(ATOT,6.0,NSTEP,1)
C      IF (SAS.EQ.0) CALL SCALE(ASUB,6.0,NSTEP,1)
C      IF (SAS.EQ.-1) CALL SCALE(ASUB,6.0,NSTEP,1)
C      CALL AXIS(0.0,0.0, 'XURLES SINCE START OF SPILL',-26,6.0,0.0,0.
C      1 TISE(SB-1),TISE(SB))
C      IF (SAS.EQ.1) TOT1 = ATOT(SB-1)
C      IF (SAS.EQ.1) TOT2 = ATOT(SB)
C      IF (SAS.EQ.0) TOT1 = ASUB(SB-1)

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Figure VII.-7. PLOTAREA

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//CODCAT92 JOB (EIA100), 'RAMER-PLT8082', TIME=(1)
//JOBPARM LINES=10
// EXEC SCDD58,DSB='DRI.EIA1.PLT908'
// EXEC BEALOC
//POST DD DS=ORIG.EIA1.PLT808,SPACE=(TRF,(2,2)),
// DISP=(NEW,CATLG),UNIT=STSDA,
// DCB=(RECFM=VBS,BLKSIZE=1954)
// EXEC PGM=CCG,LIB=CPL0T,REGION=CO=128K,
// PRT=SI500*(C,,2019),P3=SI500*(C,,2019)
// PRT=SI510 DD *
C
C THIS PROGRAM PLOTS AN AERIAL VIEW OF THE LOCATION OF
C THE SPILLLETS AND THE SUBSURFACE POSITION. IT FIRST
C DETERMINES THE MAXIMUM AND MINIMUM EXTENT (IN LONGITUDE
C AND LATITUDE IF ISCAL=2 AND IF GETTERS FROM THE (1,1)
C POSITION IF ISCAL=1). THESE ARE THEN USED TO DETERMINE
C THE ORIGIN AND SCALE OF THE PLOT.
C.....
C CORROK /POST/ EDL, YDL, AD, SCAL, EOP, YOP
C INTGEP VECT08(3),31
C DIMENSION IG(799),IC(799),CG(799)
C
C BCK = 0
C CONTINUE
C
C CALL READI(HPLOT, 'HPLOT', 1, 2)
C CALL READI(HSTEP, 'HSTEP', 1, 50)
C CALL READI(RP, 'RP', 1)
C CALL READI(TWICK, 'TWICK', 1)
C CALL READI(TLKG, 'TLKG', 1)
C CALL READI(TVLT, 'TVLT', 1)
C CALL READI(EPOIC, 'EPOIC', 0, 1)
C CALL READI(ISCAL, 'ISCAL', 1, 2)
C CALL READI(ENROT, 'ENROT', 0, 1500)
C
C READ IN DATA AND DETERMINE THE BARRIOR EXTENTS
C
C DO 32 J=1,HPLOT
C DO 32 JP=1,HSTEP
C READ(KB) IDAT,TIME,ESPIL
C
C RETAIN INITIAL SPILLLET POSITION TO KEEP TO
C
C DO 47 I=1,ESPIL
C READ(KB) ESP,TSP,TRIC
C IF(ENROT.EQ.1) GO TO 84
C ISF = TSP
C IRAI = ISF
C ISIT = TSP
C YRII = TSP
C YRAI = TSP
C YSII = TSP
C YSAI = TSP
C WRITE(6,55) ISIT,YSIT
C FORAM(21,'SITE',2F10.3)
C BCK = 1
C CONTINUE
C ESP = ESP/(1.142E 05)
C
C ISPL = ISF + ESP
C ISPD = ISF - ESP
C ISL = ISF - ISI
C YSPD = ISF + ESP
C YSP = ISF - ISF
C IF(ISCAL.EQ.1) IRAI = ISPL
C IF(ISCAL.EQ.1) IRAI = ISPD
C IF(ISCAL.EQ.1) YRAI = ISPL
C IF(ISCAL.EQ.1) YRAI = ISPD
C CONTINUE
C IF(ENROT.EQ.0) GO TO 32
C
C READ IN SUBSURFACE INFORMATION,
C BUT NOT THE FIRST STEP
C
C READ(KB) IRS,ISI,VNS,YSI,DI,DT,SUBSELN,AD,IDL,YDL
C IF(TIME.EQ.0.0) WRITE(6,333) AD
C FORAM(21,' ANGLE IS',F10.3)
C IF(AD.EQ.0.0) GO TO 667
C CALL POSIT(IRS,YSI,YSI,YSI,1)
C IF(IRS.EQ.1) IRAI=ISI
C IF(IRS.EQ.2) IRAI=YSI
C IF(IRS.EQ.3) IRAI=YSI
C IF(IRS.EQ.4) IRAI=YSI
C CALL POSIT(IRS,YSI,YSI,YSI,1)
C IF(IRS.EQ.1) IRAI=ISI
C IF(IRS.EQ.2) IRAI=YSI
C IF(IRS.EQ.3) IRAI=YSI
C IF(IRS.EQ.4) IRAI=YSI
C CALL POSIT(IRS,YSI,YSI,YSI,1)
C IF(IRS.EQ.1) IRAI=ISI
C IF(IRS.EQ.2) IRAI=YSI
C IF(IRS.EQ.3) IRAI=YSI
C IF(IRS.EQ.4) IRAI=YSI
C CALL POSIT(IRS,YSI,YSI,YSI,1)
C IF(IRS.EQ.1) IRAI=ISI
C IF(IRS.EQ.2) IRAI=YSI
C IF(IRS.EQ.3) IRAI=YSI
C IF(IRS.EQ.4) IRAI=YSI
C GO TO 776
C CONTINUE
C IF(IRS.EQ.1) IRAI = IRS
C IF(IRS.EQ.2) IRAI = ISI
C IF(IRS.EQ.3) IRAI = YSI
C IF(IRS.EQ.4) IRAI = YSI
C CONTINUE
C DO 31 I = 1,SUBSELN
C READ(KB) IC,IC,CC
C CONTINUE
C CONTINUE
C YIRDAI = TIME
C
C BEHIND DATA SETS
C
C DO 64 JJ = 1,HPLOT
C BEHIND JJ
C CONTINUE
C
C WRITE(6,910) ISIT,IRAI,YSI,YSI
C FORAM(21,' BARRIOR LONGITUDE IS',F6.2,' BARRIOR LONGITUDE',
C ' IS',F6.2,'/21,' BARRIOR LATITUDE IS',F6.2,

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2 ' BARRIOR LATITUDE IS',F6.2)
C
C DETERMINE THE MAXIMUM SPREAD OF THE OIL AND
C THEN DIVIDE THE SPACING BY 10 AND LEAVE 1.5
C OF THESE DIVISIONS ON THE OUTSIDE OF THE PLOT.
C THIS WILL GIVE THE ORIGIN OF ALL OF THE ISSUING
C PLOTS AS WELL AS DETERMINING A SCALE FACTOR TO
C CONVERT FROM DEGREES TO INCHES.
C
C IDIF = IRAI - ENAI
C YDIF = YRAI - ENAI
C DI = IDIF/10.0
C YDI = YDIF/10.0
C SLOP = YDI / DI
C YOP = YRII - 1.5*DI
C EOP = (IRAI+ENAI)/2.0
C YLAT = (YRAI+ENAI)/2.0
C EDEG = DI * 13.0
C YDEG = DI * 13.0
C XDEG = XDEG / 5.5
C YDEG = YDEG / 5.5
C EDCT = XDEG/COS(YLAT/57.296)
C SCAL = EDCT
C IF(DCT.GT.SCAL) SCAL = EDCT
C WRITE(6,443) IDIF,EOP,SCAL
C FORAM(21,' SCAL FACTORS ARE',3F12.5)
C
C WRITE OUT THE ORIGIN OF THIS PLOT
C
C WRITE(6,911) EOP,YOP
C FORAM(21,' THE ORIGIN OF THIS PLOT IS',F6.2,' Y',F6.2,' X')
C
C DO LOOP OVER THE STEPS AND DATA SETS
C
C CALL PLOTS(0,0,8)
C CONTINUE
C DO 35 JJ = 1,HPLOT
C CONTINUE
C
C USE BLACK FOR PLOTTING OUTLINE
C
C SET UP THE FIRST MAP
C
C READ(JJ) IDAT, TIME, ESPIL
C
C END IF TIME HAS BEEN PASSED
C
C IF((TIME.GT.TIMEAR).AND.(JJ.EQ.HPLOT)) GO TO 2121
C
C IS THIS A HOUR WE'RE INTERESTED IN?
C
C CREC = AROD(TIME,RP)
C IF(CREC.EQ.0) GO TO 35
C
C READ IN DATA ALTHOUGH THIS STEP WILL NOT BE PLOTTED
C
C CONTINUE
C DO 3 I=1,ESPIL
C
C READ(JJ,END=2121)IDUR,TDUA,ZDUR,TBIC
C CONTINUE
C IF(ENROT.EQ.0) GO TO 89
C READ(JJ,END=2121)IOLNR,IOLBR,IOLLR,IOLNR,DI,DT,MUSELN,
C AD,IDL,YDL
C
C DO 5 I=1,SUBSELN
C READ(JJ,END=2121) ICUR,ICDB,CCDB
C CONTINUE
C CONTINUE
C GO TO 21
C CONTINUE
C
C WRITE OUT TIME AND DAY
C
C WRITE(6,99) IDAT,TIME
C FORAM(21,' THIS RUN STARTED ON DAY',I4,' AND IT IS',F6.2,
C ' HOURS AFTER THE START OF THE SPILL/')
C
C THIS SECTION PLOTS THE LEGEND.
C
C I = 0.5
C Y = 4.52
C CALL SYMBOL(X=1.0,Y=0.75,0.1,' SPILL SITE',0.0,13)
C DT = 4.0 * DT = 6371.0*3.14159/180.0
C IPT = DT * 0.5
C DT = IPT/(DI*Y)
C DIST = DT/SCAL = (180.0/(6371.0*3.14159))
C IR = I - .6
C Y = Y - .92
C CALL PLOT(1F,Y,3)
C CALL PLOT(1F,Y,1,2)
C CALL PLOT(1F,Y,3)
C CALL PLOT(1F+DIST,Y,2)
C CALL PLOT(1F+DIST,Y,0,1,2)
C I = I - 0.7
C Y = Y + 0.2
C CALL SYMBOL(1F,0.1,DT,0.0,-1)
C CALL SYMBOL(1F,0.1,1,' KILOMETERS',0.0,15)
C CALL SYMBOL(1F,0.1,1,' KILOMETERS',0.0,15)
C CALL SYMBOL(3.75,Y-0.4,0.1,' SURFACE SPILLLETS',0.0,17)
C CALL SYMBOL(3.5,Y-0.6,0.1,0.1,0.0,3)
C CALL SYMBOL(3.75,Y-0.6,0.1,' SUBSURFACE',0.0,11)
C Y = Y - 0.38
C CALL PLOT(1F,0.4,3)
C CALL PLOT(1F,0.75,1-0.4,2)
C CALL SYMBOL(1F,0.76,Y-0.4,0.1,' CASE 1',0.0,7)
C IF(HPLOT.EQ.1) GO TO 664
C CALL PLOT(1F,0.6,3)
C CALL DISRP(1F,0.75,Y-0.4,0.05)
C CALL SYMBOL(1F,0.76,Y-0.6,0.1,' CASE 6',0.0,7)
C CONTINUE
C CALL PLOT(3.4,5.5,3)
C CALL PLOT(3.4,3.9,2)
C CALL PLOT(5.5,3.9,2)
C
C PLOT RECTANGLES AROUND PLOT
C
C CALL RECT(-0.75,-0.75,7.0,7.0,0.0,3)
C CALL RECT(0.0,0.0,5.5,5.0,0.0,3)

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Figure VII.-8. PLOTMAP

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CALL BORDER(-0.9,7.0,0.21,TIME,0.0,1)
CALL STROB(-0.1,7.0,0.21,' BODAS AFTER START OF THE SPILL',
0.0,31)
CALL STROB(-0.60,6.5,0.21,' SAP OF SPILLET'S ARE SUBSURFACE',
0.0,31)
C
C DETERMINE MIBRUS LONGITUDE AND LATITUDE TO THE
C NEXT TURNS FOR PLOTTING
C
CALL PLOT(2.75,0.0,-3)
C
C PLOT SPILL SIZE AND LONGITUDES AND LATITUDES
C
Y=(YSIT-YOP)/SCAL
X=(XOP-ESIT)/SCAL
RAD=YSIT*3.14159/180.0
R=COS(RAD)
CALL STROB(1-0.12,7-0.15,0.3,*,*,0.0,1)
ZOP = 10.0*(ZOP+0.05)
IS = FLOAT(ZOP)/10.0 + 1.0
ILB1 = IS
ILB2 = IS
IB1 = (ZOP - IS)/SCAL
IB2 = IS1
ITOP=10.0*(ZOP+0.05)
IS = FLOAT(ITOP)/10.0 - 1.0
ILT1 = IS
ILT2 = IS
IXT = 10.0 * (XDIF*(3.0*DI1))/0.1
ITY = 10.0 * (YDIF*(3.0*DI1))/0.1
IP1 = (IS - YOP)/SCAL
IP2 = (IS - ZOP)/SCAL
DO 34 J=1,ITZ
JJ = J - 1
BCB = ARND(FLOAT(JJ),ILB2)
ID = -0.08
IF(BCB.EQ.0) ID = -0.11
IF(BCB.EQ.1) ID = COS(PI*57.296)
IF(BCB.GT.2.7),01,(BCB.LT.-2.7)) GO TO 92
CALL PLOT(IPF,0.00,3)
CALL PLOT(IPF,7.2)
IF(BCB.EQ.0) CALL BORDER(IPF-0.25,-0.25,0.12,ILB1,0.0,1)
CONTINUE
92 CONTINUE
IB1 = IB1 + 0.1/SCAL
ILB1 = ILB1 - 0.1
34 CONTINUE
DO 36 J=1,ITZ
JJ = J - 1
BCB=ARND(FLOAT(JJ),ILB2)
ID = 5.58
IF(BCB.EQ.0) ID = 5.61
ITY = ITZ-5.5*SCAL
IBP = IB2 + COS(PI*57.296)
IF(BCB.GT.2.7),01,(BCB.LT.-2.7)) GO TO 96
CALL PLOT(IPF,5.5,3)
CALL PLOT(IPF,7.2)
IF(BCB.EQ.0) CALL BORDER(IPF-0.25,5.64,0.12,ILB2,0.0,1)
CONTINUE
96 CONTINUE
IB2 = IB2 + 0.1/SCAL
ILB2 = ILB2 - 0.1
36 CONTINUE
DO 38 J=1,ITZ
JJ = J - 1
IF((IB1.GT.5.49),01,(IB1.LT.0.01)) GO TO 93
BCB = ARND(FLOAT(JJ),ILB2)
IL = -2.83
IF(BCB.EQ.0) IL = -2.81
CALL PLOT(-2.75,7.1,3)
CALL PLOT(IL,7.1,2)
IF(BCB.EQ.0) CALL BORDER(-3.33,7.1-0.06,0.12,ILT1,0.0,1)
CONTINUE
93 CONTINUE
IB1 = IB1 + 0.1/SCAL
ILT1 = ILT1 - 0.1
38 CONTINUE
DO 36 J=1,ITZ
JJ = J - 1
BCB=ARND(FLOAT(JJ),ILT2)
IF((IB2.GT.3.95),01,(IB2.LT.0.01)) GO TO 98
IB = 2.83
IF(BCB.EQ.0) IB = 2.86
CALL PLOT(2.75,7.2,3)
CALL PLOT(IL,7.2,2)
IF(BCB.EQ.0) CALL BORDER(2.86,7.2-0.06,0.12,ILT2,0.0,1)
CONTINUE
98 CONTINUE
IB2 = IB2 + 0.1/SCAL
ILT2 = ILT2 - 0.1
38 CONTINUE
C
C PLOT SHORELINE
C
IF(ASHD1.GT.0) CALL PLOTSHP(SCAL,ZOS,YOP)
C
C READ IN SPILLET LOCATIONS AND PAZS
C
DO 811 JJ=1,NPLOT
WRITE(6,875) JJ
875 POPRAT(//,31,'***** CASE ',JL,' *****')
876 WRITE(6,876)
876 POPRAT(//,51,'LONGITUDE',JL,'LATITUDE',JL,'RADIUS',
JL,'THICKNESS')
DO 19 I=1,NSPILL
READ(JJ) ISPL,YSPL,ISPL,YSPL,THIC
WRITE(6,874) ISPL,YSPL,ISPL,YSPL,THIC
874 POPRAT(21,2710.3,21,710.3,710.6)
IF(THIC.LT.THICK) GO TO 19
TSP = ISPL
ISPL=ISPL-YOP
ISPL=ISPL-YOP
BAD = TSP*3.14159/180.0
ISPL=ISPL*COS(PAD)
RSPIL = RSPIL/(1.112 05)
C
C PLOT SPILLET'S AS CIRCLES
C
EPT=ISPL + RSPIL
VPT=ISPL - RSPIL
EPT = EPT/SCAL
VPT = VPT/SCAL
RSPIL = RSPIL/SCAL
CALL CIRC(EPT,VPT,0.0,360.0,RSPIL,RSPIL,1)

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19 CONTINUE
C
C IF(BRD10.EQ.0) GO TO 97
DO 11 I=1,200
CG(I)=0.0
C
C
DO 12 I=1,31
DO 12 J=1,31
12 VECTOR(I,J)=0.0
READ(JJ,END=2121)ZOILB,ZOILR,ZOILR,DIT,DIT,MURIL,
1 81,IDL,YOL
WRITE(6,827)MURIL
827 POPRAT(//,,' THERE ARE',JL,' CONCENTRATION VALUES OUT THERE,')
C
C IF(AD.BE.0.0) GO TO 91
DIT = DIT/(1.112 05)*SCAL
DIT = DIT/(1.112 05)*SCAL
YLAT=(YOILR-YOILB)/2.0
YOILB = (YOILB-YOP)/SCAL
YOILR = (YOILR-YOP)/SCAL
ZOILB = ZOP-YOILB
ZOILR = ZOP-YOILR
BAD = YLAT*3.14159/180.0
ZOILB = ZOILB*COS(PAD)/SCAL
ZOILR = ZOILR *COS(PAD)/SCAL
91 CONTINUE
C
C READ IN GRID LOCATIONS AND CONCENTRATIONS
C
WRITE(6,822)
822 POPRAT(67,'LONGITUDE',JL,'LATITUDE',JL,'PARTS/BILLION')
DO 50 I=1,NOSILN
READ(JJ,END=2121)IG(I),YG(I),CG(I)
822 WRITE(6,831) IG(I),YG(I),CG(I)
831 POPRAT(71,3712.3)
IF(AD.BE.0.0) GO TO 50
YGC = YG(I)
IG(I)=(YGC(I)-YOP)/SCAL
CG(I)=CG-IG(I)
BAD = YGC*3.14159/180.0
IG(I)=IG(I)*COS(PAD)/SCAL
50 CONTINUE
C
C FOR SOFT TBC BARS OF VECTOR STARTING IN THE NORTH
C
YLATR=YOILR
DO 70 I=1,31
DO 68 J=1,NOSILN
IF(ABS(YG(J)-YLATR),LT.(DIT/3.0)) GO TO 65
GO TO 68
65 CONTINUE
C
C IT'S IN THE ITH ROW, SO NOW LOCATE THE COLUMN
C
DO 67 K=1,31
PERIS=FLOAT(K-1)
DELTAI=PERIS*0.12 + ZOILB
IF(ABS(DELTAI-IG(J)),LT.(DIT/3.0)) VECTOR(I,K)=1
67 CONTINUE
68 CONTINUE
68 CONTINUE
YLATRI=YLATRI - DIT
70 CONTINUE
C
C NOW ALL THE 1'S AND 0'S SHOULD BE IN PLACE
C
DO 72 I=1,31
72 WRITE(6,861) (VECTOR(I,J),J=1,31)
861 POPRAT(3122)
C
C SO PLOT THE SUBSURFACE OIL OUTLINES, WEST SIDE FIRST, GOING CCW
C
DO 85 I=1,31
DO 85 J=1,30
JPLUS=J+1
IFPLUS=1
EDIST=ZOILB - DIT/2.0 + DIT*FLOAT(J)
VDIST=YOILB - DIT/2.0 -DIT*FLOAT(I-1)
EPL = EDIST
VPL = VDIST
IF(VECTOR(I,J).EQ.VECTOR(I,JPLUS))GO TO 75
C
C HERE TO PUT A VERTICAL BETWEEN THEM
C
IF(AD.BE.0.0) CALL POSIT(EDIST,VDIST,EPL,VPL,0)
CALL PLOT(EPL,VPL,3)
EPL = EDIST
VPL = VDIST-DIT
IF(AD.BE.0.0) CALL POSIT(EPL,VPL,EPL,VPL,0)
IF(JJ.EQ.1) CALL PLOT(EPL,VPL,2)
IF(JJ.EQ.2) CALL DASHP(EPL,VPL,0.05)
C
75 IF(VECTOR(I,J).EQ.VECTOR(IPLUS,J)) GO TO 76
IF(1.EQ.31.AND.VECTOR(I,J).EQ.0) GO TO 76
C
C MAKE FOR A HORIZONTAL
C
EPL = EDIST-DIT
VPL = VDIST-DIT
IF(AD.BE.0.0) CALL POSIT(EPL,VPL,EPL,VPL,0)
CALL PLOT(EPL,VPL,3)
EPL = EDIST
VPL = VDIST
IF(AD.BE.0.0) CALL POSIT(EPL,VPL,EPL,VPL,0)
IF(JJ.EQ.1) CALL PLOT(EPL,VPL,2)
IF(JJ.EQ.2) CALL DASHP(EPL,VPL,0.05)
C
76 IF(1.EQ.1.AND.VECTOR(I,J).EQ.1.OR.1.EQ.31.AND.VECTOR(I,J).EQ.1)
GO TO 77
GO TO 78
77 CONTINUE
EPL = EDIST-DIT
VPL = VDIST
IF(AD.BE.0.0) CALL POSIT(EPL,VPL,EPL,VPL,0)
CALL PLOT(EPL,VPL,3)
EPL = EDIST
VPL = VDIST
IF(AD.BE.0.0) CALL POSIT(EPL,VPL,EPL,VPL,0)
IF(JJ.EQ.1) CALL PLOT(EPL,VPL,2)

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Figure VII.-8. PLOTMAP


```

78 IF(JJ.EQ.2) CALL DASHP(IPL,YPL,0.05)
   IF(J.EQ.1.AND.VECTOR(1,J).EQ.1) GO TO 79
   GO TO 81
79 CONTINUE
   XPL = XDIST-DIT
   YPL = YDIST
   IF(AD.WE.0.0) CALL POSIT(XPL,YPL,XPL,YPL,0)
   CALL PLOT(XPL,YPL,3)
   XPL = XDIST-DIT
   YPL = YDIST-DIT
   IF(AD.WE.0.0) CALL POSIT(XPL,YPL,XPL,YPL,0)
   IF(JJ.EQ.1) CALL PLOT(XPL,YPL,2)
   IF(JJ.EQ.2) CALL DASHP(IPL,YPL,0.05)
81 IF(J.EQ.31.AND.VECTOR(1,J).EQ.1) GO TO 82
   GO TO 85
82 CONTINUE
   XPL = XDIST
   YPL = YDIST
   IF(AD.WE.0.0) CALL POSIT(XPL,YPL,XPL,YPL,0)
   CALL PLOT(XPL,YPL,3)
   XPL = XDIST
   YPL = YDIST-DIT
   IF(AD.WE.0.0) CALL POSIT(XPL,YPL,XPL,YPL,0)
   IF(JJ.EQ.1) CALL PLOT(XPL,YPL,2)
   IF(JJ.EQ.2) CALL DASHP(IPL,YPL,0.05)
85 CONTINUE
97 CONTINUE
811 CONTINUE
C
   CALL PLOT(9.0,0.0,-3)
   IF(TIME.LT.TIRBAZI) GO TO 74
2121 CONTINUE
   CALL PLOT(0.0,0.0,999)
   STOP
   END
   SUBROUTINE POSIT(XD,TO,IF,YP,UCH)
C
C THIS SUBROUTINE CONVERTS THE POSITIONS EG, YC, WHICH
C ARE GIVEN RESPECT TO THE DEPTH CENTER TO A
C POSITION IN LONGITUDE AND LATITUDE AND THEN
C TO PLOTTING UNITS (INCHES) IF UCH=0.
C
C.....
C CCMAX /PCST/ XEL, YDL, AD, SCAL, ECF, YCF
C
C   X = XD * COS(-AD) + TO * SIN(-AD)
C   Y = XD * SIN(-AD) + TO * COS(-AD)
C
C CONVERT FROM METERS TO DEGREES
C
C   YP = YDL * 180 / (3.14159 * 6370)
C   XAD = YP / 57.296
C   XP = XDL - XAD / (3.14159 * 6370 * COS(XAD))
C   IF(MCH.WE.0) RETURN
C   XP = (XDL - XAD) / SCAL
C   YP = (YP - YDL) / SCAL
C   IF = (YP - YDL) / SCAL
C   RETURN
C   END
C   SUBROUTINE READ1(I,IBASE,IL,BO)
C
C   REAL*8 IBASE, IPRANE
C   DATA N1,N2 /5,6/
C   READ (N1,10) I, IPRANE
C   FORMAT(15,5I,18)
10 IF(IPRANE.EQ.IBASE) GO TO 100
   WRITE (N2,20) IPRANE, IBASE
20 FORMAT(21X CARDS OUT OF ORDER ,A8,6X READ ,A8,10X REQUESTED)
100 CONTINUE
   IF(IL.EQ.BO) GO TO 200
   IF( (I.GE.N1) .AND. (I.LE.N2) ) GO TO 200
   WRITE (N1,40) IPRANE, IL, N1, IBASE, I
40 FORMAT(16X THE LIMITS ON ,A8,5X ARE ,15,4X TO ,15,
   1 6X BUT ,A8,16X WAS READ IN AS ,15)
   STOP
200 CONTINUE
   WRITE (N1,30) I, IPRANE
30 FORMAT(21,15,5I,18)
   RETURN
   END
   SUBROUTINE READP(I, IPRANE)
   REAL*8 IPRANE, IPRANE
   DATA N1,N2 /5,6/
   DATA ISCALE / 2/
10 READ (N1,10) I, IPRANE
   FORMAT(15,5I,18)
   IF(IPRANE.EQ.IPRANE) GO TO 100
   WRITE (N1,20) IPRANE, IPRANE
20 FORMAT(21X CARDS OUT OF ORDER ,A8,6X READ ,A8,10X REQUESTED)
   STOP
100 WRITE (N1,30) I, IPRANE
30 FORMAT(21,15,5I,18)
   RETURN
   END
   SUBROUTINE PLYSH( SCAL, XOP, YOP)
C
C SUBROUTINE DESCRIPTION
C
C THIS SUBROUTINE PLOTS THE COASTLINE.
C
C.....
C
C DIRECTION STATEMENTS
C
C DIRECTION ISHOR(1495), YSHOF(1495)
C
C S T A P T B L I E
C
C INITIALIZE VARIABLES.
C
C   XP(IPASS.EQ.1) GO TO 500
C
C   BPTS = 1495
C   READ (2) ISHOR
C   READ (2) YSHOF
C   RETURN 2
500 CONTINUE

```

```

C
C NO OVER SHOPELINE POINTS.
C
C   DO 99 IPT=1,BPTS
C   IF(ISHOF(IPT).GT.0.0) GO TO 110
C   BPLC1 = 1
C   GO TO 99
110 CONTINUE
C
C CALCULATE THE SHOPE POINT IS CALCORP INCHES.
C
C   IPT = (XOP - ISHOR(IPT)) * COS(TSHOF(IPT)) + 3.14159 / 180.0
C   / SCAL
C   YPT = (YSHOF(IPT) - YOP) / SCAL
C
C IS THIS POINT OUT OF RANGE IN X?
C
C   IF( (IPT.GT.-2.75) .AND. (IPT.LT.2.75) ) GO TO 120
C   BPLC1 = 1
C   GO TO 100
120 CONTINUE
C
C IS THIS POINT OUT OF RANGE IN Y?
C
C   IF( (YPT.GT.0.1) .AND. (YPT.LT.5.5) ) GO TO 130
C   BPLC1 = 1
C   GO TO 100
130 CONTINUE
C
C IS THIS POINT IN THE LABEL BOX?
C
C   GO TO 140
C   IF( (IPT.LT.-.65) .OR. (YPT.LT.-.125) ) GO TO 140
C   BPLC1 = 1
C   GO TO 100
140 CONTINUE
C
C CHECK FLAGS AND DRAW TO (IPT,YPT) IF EQUIPPED.
C
C   IF(BPLC1.EQ.1) GO TO 150
C   IF(IPT.EQ.1) GO TO 150
C   CALL PLOT( IPT, YPT, 2)
C
C
C SKIP TO LOCATION (IPT,YPT).
C
C
150 CONTINUE
   BPLC1 = 0
   CALL PLOT( IPT, YPT, 3)
   CONTINUE
   ILST = IPT
   YLST = YPT
99 CONTINUE
C
C B E T W E E N B I F F
C
C   RETURN
C   END
//GO.STRIP DD *
   1 PLOT

```

```

10 BSTEP
3.000 BE
0.00 TRICK
10.00 MLC
5.00 YLTD
1 BBD10
2 ISCAL
0 BSHOF
//GO.PT08P001 DD DSH=UFI.EIA1.PLTRON,DISP=OLD
//GO.PT01P001 DD BSH=ORL.EIA1.BEBUC.COT50,DISP=SHR
//GO.PT02P001 DD BSH=ORL.EIA1.PEP75.P40350.COT50,DISP=SHR

```

Figure VII.-8. PLOTMAP


```

201 FORMAT( 'THE STANDARD DEVIATIONS ARE ',D12.3P16.6)
81 CONTINUE
C
C
C
P I C T U R E P E R E
C
C
IF( (DI,CT,0.0) .AND. (DY,CT,0.0) ) RETURN
C
C
STEP FOR AN ERROR IN THE CALCULATION OF DI OR OF DY.
C
C
WRITE(NB,110) DI, DY
110 FORMAT('O ERROR ',50(' '), ' DI=',D16.5, ' DY=',D16.5)
C
C
S T O P P E R E
C
C
STOP
END
SUBROUTINE CONC( C, I, Y, Z, WORDS)
C
C
SUBROUTINE DESCRIPTION
C
C
IN THIS SUBROUTINE THE CONCENTRATION OF NAPREP PARTICLES 2400
IS CALCULATED IN EACH OF THE FLOATING GRID CELLS.
C
C
.....2400
C
COMMON STATEMENTS
C
COMMON /CMTL/ INSDI, JNSDI, PMSDI, HPTA,
1 DI, TIME, ISCAL, BOPCH, BOPBT
COMMON /PTYP/ WCLASS, BOPND(200), DDIAI(200), DDPND(200),
1 DRASS(200), DVELI(200), DCONP(200,8), WCLASS
COMMON /SUBS/ SBTTP, BRAI, BRAT, DI, DY, DZ,
1 DIBIC, DIBIC, DIBIC
COMMON /DPCM/ IDL, TDL, FDS, TDS
COMMON /PART/ KPPTC, KPPTI, SPRL, SPRC, WPPP
C
C
DIMENSION STATEMENTS
C
DIMENSION C(30,30,10)
DIMENSION I(8,8), I(8,8), I(8,8), I(8,8)
INTEGER*2 BOPND(8,8)
DATA W / 6 /
C
C
S T A P T P E R E
C
INITIALIZE THE CONCENTRATION ARRAY
C
C
DO 111 I=1, I=500
DO 111 J=1, J=500
DO 111 K=1, K=500
111 C(I,J,K)=0.0
C
DO LOOP OVER ALL NAPREP PARTICLES
C
DO 100 N=1, N=1
IF( I(N), I(N), O, O, I(N), I(N), I(N), I(N), I(N), I(N), I(N), I(N) ) GO TO 100
NIT = DI
DIT = DY
IF( ISCAL.EQ.1 ) GO TO 75
SCALE = (6371.0*1000.0*3.14159) / 180.0
C
C
TPAP = TOS*TORIG*Y(N) + (YDL-TDS)
DI = DI * SCALE
DI = DI * (SCALE * COS( TPAP / 37.2964))
75 CONTINUE
C
OBTAIN THE VOLUME OF A GRID ELEMENT
C
DSO = DI*DI*DI
C
OBTAIN THE MASS DENSITY PER UNIT VOLUME. END IS IN
REPPIC TONS PER CUBIC METER OF MILLIGRAMS PER MILLILITER. 2400
C
II = BOPND(I)
IND = DRASS(II) / DSO
C
OBTAIN THE SUBSCRIPTS FOR THE GRID ELEMENT FOR THIS PARTICLE 2400
C
PI = I(N) / DI
IP = PI + 1
PJ = J(N) / DI
JP = PJ + 1
PK = K(N) / DI
KP = PK + 1
C
OBTAIN THE XYZ POSITION OF THE NAPREP RELATIVE TO CELL CENTER 2400
C
XP = PI - FLOAT(IP) + 0.5
YP = PJ - FLOAT(JP) + 0.5
ZP = PK - FLOAT(KP) + 0.5
C
OBTAIN THE SUBSCRIPTS OF THOSE ELEMENTS AFFECTED BY THIS NAPREP
NAP, AYP AND AZP ARE THE ABSOLUTE VALUES OF XP, YP AND ZP 3100
C
1 IP(IP), 1,2,2
2 IO = IP - 1
3 AYP = -YP
4 IO = IP + 1
5 AYP = YP
6 CONTINUE
7 IP(IP), 0,5,5
8 JO = JP - 1
9 AYP = -YP
10 JO = JP + 1
11 AYP = YP
12 CONTINUE
13 IP(IP), 7,8,8
14 KP = KP - 1
15 AYP = -ZP
16 GO TO 9
17 KP = KP + 1
18 AYP = ZP
19 CONTINUE
C
CALCULATE THE ABSOLUTE DISTANCE OFFCENTER FOR THIS NAPREP
C
SO = 1.0 - AYP
TO = 1.0 - AYP
BO = 1.0 - AYP

```

```

C
MULTIPLY AYP AND SO BY END TO AVOID MULTIPLICATIONS LATER
C
AYP = END * AYP
SO = END * SO
C
MARK ALL SUBSCRIPTS WHICH ARE OUT OF RANGE
C
L1 = 0
L2 = 0
L3 = 0
L4 = 0
L5 = 0
L6 = 0
IF( (IP,CT,INSDI) .OR. (JP,LT,1) ) L1 = 1
IF( (IO,CT,INSDI) .OR. (IO,LT,1) ) L2 = 1
IF( (JP,CT,JNSDI) .OR. (JP,LT,1) ) L3 = 1
IF( (JO,CT,JNSDI) .OR. (JO,LT,1) ) L4 = 1
IF( (KP,CT,PMSDI) .OR. (KP,LT,1) ) L5 = 1
IF( (KO,CT,PMSDI) .OR. (KO,LT,1) ) L6 = 1
C
ADD CONCENTRATION DUE TO THIS NAPREP
C
IF( (L1.EQ.1) .OR. (L2.EQ.1) .OR. (L5.EQ.1) ) GO TO 10
C( IP, JP, KP ) = C( IP, JP, KP ) + IC * IC * IC
10 IF( (L2.EQ.1) .OR. (L3.EQ.1) .OR. (L5.EQ.1) ) GO TO 11
C( IO, JP, KP ) = C( IO, JP, KP ) + AYP * TO * IC
11 IF( (L3.EQ.1) .OR. (L4.EQ.1) .OR. (L5.EQ.1) ) GO TO 12
C( IP, JO, KP ) = C( IP, JO, KP ) + TO * AYP * IC
12 IF( (L4.EQ.1) .OR. (L5.EQ.1) .OR. (L6.EQ.1) ) GO TO 13
C( IP, JP, KO ) = C( IP, JP, KO ) + IC * IC * AYP
13 IF( (L5.EQ.1) .OR. (L6.EQ.1) .OR. (L6.EQ.1) ) GO TO 14
C( IO, JO, KP ) = C( IO, JO, KP ) + AYP * AYP * IC
14 IF( (L6.EQ.1) .OR. (L6.EQ.1) .OR. (L6.EQ.1) ) GO TO 15
C( IO, JP, KO ) = C( IO, JP, KO ) + AYP * TO * AYP
15 IF( (L6.EQ.1) .OR. (L6.EQ.1) .OR. (L6.EQ.1) ) GO TO 16
C( IP, JO, KO ) = C( IP, JO, KO ) + IC * AYP * AYP
16 IF( (L6.EQ.1) .OR. (L6.EQ.1) .OR. (L6.EQ.1) ) GO TO 17
C( IO, JO, KO ) = C( IO, JO, KO ) + AYP * AYP * AYP
17 CONTINUE
100 CONTINUE
C
P I C T U R E P I N T
C
C
PCTOP
END
SUBROUTINE PRINT( C, N, I, Y, Z, BOPND, DST, CC, WPPFLY, WPPANS)
C
SUBROUTINE DESCRIPTION
C
THIS SUBROUTINE HANDLES ALMOST ALL OUTPUT OPERATIONS.
C
.....60
C
COMMON STATEMENTS
C
COMMON /CMTL/ INSDI, JNSDI, PMSDI, HPTA,
1 DI, TIME, ISCAL, BOPCH, BOPBT,
1 DI, TIME, ISCAL, BOPCH, BOPBT
C
DIMENSION STATEMENTS
C
DIMENSION C(30,30,10)
DIMENSION DPLT(30,30), WPLT(30,30), CC(30,30)
DIMENSION I(8,8), I(8,8), I(8,8), I(8,8)
DIMENSION BOPND(8,8), BTD(30)
INTEGER*2 BOPND(8,8)
DATA W / 6 /
C
S T A P T P E R E
C
DO 44 I=1, 10
DO 44 J=1, 30
DPLT(I,J)=0.0
DPLT(I,J)=10.0
44 CONTINUE
C
PRINT 3-D CONCENTRATION FIELD AT EACH LEVEL
C
NOTE: C IS IN REPPIC TONS OF OIL PER CUBIC METR OF WATER.
CC IS PRINTED ONLY AS MG OIL PER ML WATER.
THIS IS A FACTOR OF 1000, ALSO CC IS IN
PARTS PER THOUSAND.
C
IF( (HPTA.EQ.0) .OR. (HPTA.EQ.1) ) GO TO 16
TST = ANOD( FLOAT(NST), FLOAT(FPCTC))
IF( TST.EQ.0.0 ) GO TO 16
CALL OPIDEX( I, Y, Z, DST, BPTPLI)
CALL CON( C, I, Y, Z, WPPNS)
C
FIND THE DISTANCE FROM ORIGIN OF FIELD SYSTEM TO GRID LOCATION
C
ELL = EONIC + EDS - 0.5*DT
TLL = TORIG + TDS - 0.5*DT
DO 150 I=1, INSDI
TLL = TLL - DI
150 RIO(I) = TLL
DO 160 J=1, JNSDI
TLL = TLL - DI
160 RJN(J) = TLL
DO 170 K=1, PMSDI
BPTP( (8,17) ) DST, TIME K
FORMAT( //, 'OIL CONCENTRATION IN MG OF OIL PER ML OF WATER',
1 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
2 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
3 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
4 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
5 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
6 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
7 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
8 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
9 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
10 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
11 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
12 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
13 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
14 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
15 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
16 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
17 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
18 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
19 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
20 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
21 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
22 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
23 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
24 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
25 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
26 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
27 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
28 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
29 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
30 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
31 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
32 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
33 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
34 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
35 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
36 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
37 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
38 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
39 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
40 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
41 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
42 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
43 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
44 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
45 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
46 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
47 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
48 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
49 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
50 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
51 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
52 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
53 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
54 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
55 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
56 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
57 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
58 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
59 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )
60 ' DI, TIME = ', D16.5, ' TIME = ', D16.5, ' LEVEL = ', I4 / )

```

Figure VII.-S. Particle Program

APPENDIX VIII, A SAMPLE RUN

This Appendix presents all data input from cards and the resulting output for a complete simulation. This case simulates a 5.7 million gallon spill of an oil similar to #2 fuel oil released over a six hour period. The location of the spill is off Massachusetts near Georges Bank. The environmental data used here is a sample and is not of the actual data used for previous runs in Cornillon, et al. (1979 and 1980). Figures VIII-1 to VIII-4 present the output for these programs. The reader should refer to Figure VII-1 for the input to the program GRIDS. The output of READATA (Figures VIII-2-4) shows the wind and currents which were used for the main simulation.

The input data stream for the full simulation is illustrated in Figure VIII-5. Note that some of the environmental data sets (wind, currents, etc.) are read from disk data sets and are not shown in the input stream. The output corresponding to the input of Figure VIII-5 is illustrated in Figure VIII-6. The input stream to the Preview Run is not shown here as it is identical to that for the full simulation, figure VIII-5, with the minor exception that the control parameter NRUN is equal to 0 for the Main simulation compared to 1 for the Preview. The output for the first ten time steps of the simulation are shown in Figure VIII-7. Note that the mass balance differs between the Preview and Main simulation due to the deposited particles.

Figure VIII-8 shows the output of a sample restarted run. The sub-surface parameters of a restarted run will not be the same as a full run due to the re-initialization of the random number generator in Subroutine INJECT. The remaining figures deal with the input and resulting output for the output programs. Figures VIII-9 and VIII-10 show the printed output and resulting plot from the program PLOTMASS. The user is again referred to Appendix VII where the program listing also displays the input parameters. Figure VIII-11 is an output from DATAOUT, which shows all information which has been written out by the main program for use by DATAOUT. Figure VIII-12 shows the abbreviated output from DATAOUT which is generated for the programs PLOTMAP AND PLOTAREA. Figure VIII-13 is the output from CHECDATA which shows the full amount of data formatted by DATAOUT. Figures VIII-14 and VIII-15 shows the output and an example plot generated by the plotting program PLOTMAP. Figures VIII-16 and VIII-17 give the same for the program PLOTAREA. Figure VIII-18 shows the output from the program PARTICLE which was generated from the data in Figure VIII-11. The output is read left to right.

```

INPUT PARAMETER:
1  XPORTA
2  X0
1  X1
1  X2
1  X3
5  X4
10800.00000  X5
1  X6
5  X7
5  X8
20.00000  X9
500.00000  X10
800.00000  X11
71.75000  X12
19.75000  X13
WIND VEL  TITLE
0  WIND1
0  WIND2
0  WIND3
0  WIND4
0  WIND5

WIND VEL  GRID HAS 5 DIVISIONS IN X SPACED
AND 5 DIVISIONS IN Y SPACED
THE WIND VEL GRID LOCATION OF THE WIND VEL COORDINATE SYSTEM IS AT 71.75000 DEGREES LONGITUDE AND 19.75000 DEGREES LATITUDE.
FINALLY THE X AXIS OF THE WIND VEL GRID MAKES AN ANGLE (COUNTERCLOCKWISE) OF 20.00000 DEGREES WITH LINES OF CONSTANT LATITUDE.

U  VALUES IN UNITS OF  M /SEC
E ELEMENTS
1  2  3  4  5
5  5.  5.  5.  5.  5.
0  0.  0.  0.  0.  0.
3  3.  3.  3.  3.  3.
2  2.  2.  2.  2.  2.
1  1.  1.  1.  1.  1.

V  VALUES IN UNITS OF  M /SEC
E ELEMENTS
1  2  3  4  5
5  0.0  0.0  0.0  0.0  0.0
0  0.0  0.0  0.0  0.0  0.0
3  0.0  0.0  0.0  0.0  0.0
2  0.0  0.0  0.0  0.0  0.0
1  0.0  0.0  0.0  0.0  0.0

```

Figure VIII.-1. Sample Output from Program
Grids

```

TERRA PARAMETERS
1  WPTA
2  W1
3  W2
10 W3
1  W4
2  W5CAL

```

```

WIND SPL      TERRA DATA      0.0  WINDS  SPEEDS PER OBSERVING TO THE WIND
THE WIND SPL  GRID MAX  1 DIVISIONS IN X SPACE  0.500  WINDSPEED  SPEED
              END      1 DIVISIONS IN Y SPACE  0.250  WINDSPEED  SPEED.

THE (1,1) GRID LOCATION OF THE WIND SPL  COORDINATE SYSTEM IS AT  48.000000  DEGREES  L301E7300  AND  41.250000  DEGREES  L41E7300

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  0.0

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  -6.

WIND SPL      TERRA DATA      0.0  WINDS  SPEEDS PER OBSERVING TO THE WIND
THE WIND SPL  GRID MAX  1 DIVISIONS IN X SPACE  0.500  WINDSPEED  SPEED
              END      1 DIVISIONS IN Y SPACE  0.250  WINDSPEED  SPEED.

THE (1,1) GRID LOCATION OF THE WIND SPL  COORDINATE SYSTEM IS AT  48.000000  DEGREES  L301E7300  AND  41.250000  DEGREES  L41E7300

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  0.0

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  -6.

WIND SPL      TERRA DATA      0.0  WINDS  SPEEDS PER OBSERVING TO THE WIND
THE WIND SPL  GRID MAX  1 DIVISIONS IN X SPACE  0.500  WINDSPEED  SPEED
              END      1 DIVISIONS IN Y SPACE  0.250  WINDSPEED  SPEED.

THE (1,1) GRID LOCATION OF THE WIND SPL  COORDINATE SYSTEM IS AT  48.000000  DEGREES  L301E7300  AND  41.250000  DEGREES  L41E7300

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  -7.

      0  VALUES IN UNITS OF  W/SEC
      Y PLANNETS  1
      1  0.0

```

Figure VIII.-2. Output from READATA; Wind Speed and Direction

INPUT PARAMETERS
 1 BOWEN
 1 DO
 1 SS
 10 PDR
 1 SD
 2 INCAL

OTID CURRENT INPUT DATA 0.0 NUMBER AFTER THE RECEIPT OF THE SPILL
 THE OTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.1572-DIVISIONS APART
 AND 10 DIVISIONS IN Y SPACED 0.1572-DIVISIONS APART.
 THE (1,1) GRID LOCATION OF THE OTID CURRENT COORDINATE SYSTEM IS AT 47.00000 DEGREES LONGITUDE AND 41.30000 DEGREES LATITUDE.
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10** -6

VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10				
10	0.019	0.019	0.019	0.203	0.275	0.525	0.787	0.767	0.702	0.700	0.717	0.551	0.193	0.005
13	0.010	0.010	0.010	0.304	0.423	0.740	0.714	0.457	0.701	0.751	0.620	0.688	0.220	0.000
12	0.014	0.016	0.014	0.254	0.307	0.487	0.670	0.703	0.772	0.626	0.555	0.604	0.111	0.059
11	0.010	0.010	0.600	0.120	0.190	0.225	0.608	0.627	0.778	0.600	0.433	0.301	0.156	0.637
10	0.011	0.013	0.011	0.011	0.259	0.122	0.553	0.580	0.735	0.510	0.610	0.570	0.056	0.000
9	0.011	0.011	0.011	0.011	0.322	0.019	0.526	0.528	0.706	0.505	0.702	0.526	0.587	0.175
8	0.009	0.009	0.009	0.009	0.219	0.010	0.463	0.501	0.660	0.079	0.412	0.407	0.516	0.151
7	0.040	0.556	0.120	-0.142	0.157	0.053	0.186	0.020	0.417	0.413	0.071	0.040	0.100	0.120
6	0.050	0.300	0.160	-0.081	0.029	-0.060	0.197	0.170	0.225	0.101	0.280	0.009	0.125	0.136
5	0.004	0.006	0.199	-0.020	-0.100	-0.150	-0.150	-0.217	-0.551	-0.107	0.019	0.190	0.226	0.296
0	0.072	0.073	0.103	0.027	-0.071	-0.213	-0.012	-0.111	-0.110	-0.130	0.010	0.110	0.110	0.170
3	0.097	0.100	0.087	0.071	-0.001	-0.071	0.005	-0.006	-0.005	0.019	0.009	0.029	0.010	0.006
2	0.100	0.099	0.075	0.070	0.029	0.010	0.003	0.010	-0.010	0.010	0.013	0.070	0.037	0.000
1	0.123	0.096	0.063	0.060	0.090	0.097	0.002	0.010	0.007	-0.007	0.006	0.012	0.001	0.073

OTID CURRENT INPUT DATA 0.0 NUMBER AFTER THE RECEIPT OF THE SPILL
 THE OTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.1572-DIVISIONS APART
 AND 10 DIVISIONS IN Y SPACED 0.1572-DIVISIONS APART.
 THE (1,1) GRID LOCATION OF THE OTID CURRENT COORDINATE SYSTEM IS AT 47.00000 DEGREES LONGITUDE AND 41.30000 DEGREES LATITUDE.
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10** -6

VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10				
10	0.609	0.609	0.609	0.031	0.465	0.710	0.976	0.957	0.901	0.800	0.926	0.760	0.122	0.215
13	0.606	0.606	0.606	0.570	0.411	0.910	0.925	1.004	0.971	0.910	0.917	0.916	0.400	0.207
12	0.600	0.600	0.600	0.402	0.405	0.475	0.850	0.800	0.960	0.810	0.703	0.680	0.400	0.606
11	0.601	0.601	0.027	0.311	0.181	0.412	0.791	0.810	0.945	0.787	0.720	0.570	0.503	0.420
10	0.599	0.599	0.599	0.599	0.405	0.100	0.710	0.706	0.921	0.720	0.706	0.760	0.403	0.476
9	0.507	0.507	0.507	0.507	0.507	0.205	0.711	0.710	0.800	0.601	0.402	0.911	0.773	0.561
8	0.590	0.590	0.590	0.590	0.420	0.201	0.600	0.606	0.805	0.600	0.707	0.772	0.400	0.516
7	0.252	0.700	0.100	0.007	0.101	0.237	0.571	0.610	0.801	0.507	0.455	0.600	0.570	0.512
6	0.242	0.400	0.301	0.102	0.212	0.120	0.180	0.157	0.400	0.327	0.449	0.502	0.500	0.520
5	0.211	0.229	0.302	0.161	0.083	-0.176	0.011	-0.030	-0.170	-0.125	0.202	0.176	0.400	0.470
0	0.210	0.255	0.325	0.209	0.111	-0.031	0.150	0.071	-0.136	0.000	0.100	0.100	0.102	0.152
3	0.270	0.202	0.269	0.255	0.180	0.111	0.206	0.176	0.097	0.220	0.191	0.210	0.196	0.227
2	0.290	0.279	0.256	0.251	0.210	0.105	0.200	0.197	0.102	0.107	0.100	0.210	0.212	0.201
1	0.101	0.216	0.201	0.200	0.270	0.277	0.262	0.219	0.107	0.171	0.107	0.212	0.232	0.251

Figure VIII.-3. Output from READATA; x-direction currents

DTID CURRENT INPUT DATA 0.0 HOURS AFTER THE BEGINNING OF THE SPILL
 .OR DTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.1578-01DEGPPRS APART
 AND 10 DIVISIONS IN Y SPACED 0.1578-01DEGPPRS APART.
 THE (1,1) GRID LOCATION OF THE DTID CURRENT COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 43.140001 DEGREES LATITUDE.
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10⁻⁶

Y ELEMENTS	X ELEMENTS													
	VALUES IN UNITS OF M/S													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	0.139	0.139	0.139	-0.017	-0.005	0.245	0.507	0.487	0.512	0.478	0.456	0.271	-0.168	-0.215
13	0.138	0.138	0.138	0.107	0.141	0.470	0.457	0.578	0.503	0.472	0.349	0.369	-0.059	-0.181
12	0.138	0.138	0.138	-0.029	0.029	0.209	0.192	0.429	0.498	0.388	0.277	0.218	0.011	0.181
11	0.137	0.137	0.137	-0.153	-0.081	-0.052	0.127	0.150	0.501	0.371	0.256	0.118	0.079	0.140
10	0.137	0.137	0.137	0.117	-0.017	-0.154	0.277	0.108	0.459	0.258	0.310	0.298	0.180	0.218
9	0.136	0.136	0.136	0.116	0.087	-0.256	0.251	0.250	0.429	0.210	0.427	0.451	0.312	0.100
8	0.136	0.136	0.136	0.116	-0.035	-0.256	0.190	0.227	0.387	0.205	0.319	0.113	0.240	0.077
7	-0.205	0.283	-0.153	-0.415	-0.116	-0.220	0.118	0.157	0.188	0.140	0.199	0.212	0.121	0.055
6	-0.213	0.029	-0.112	-0.351	-0.281	-0.331	-0.075	-0.098	-0.086	-0.129	0.012	0.117	0.058	0.068
5	-0.222	-0.228	-0.071	-0.291	-0.370	-0.429	-0.420	-0.488	-0.428	-0.578	-0.252	-0.077	-0.095	0.025
4	-0.198	-0.186	-0.127	-0.282	-0.381	-0.481	-0.102	-0.181	-0.548	-0.481	-0.255	-0.160	-0.150	-0.099
3	-0.172	-0.164	-0.181	-0.196	-0.310	-0.339	-0.188	-0.275	-0.153	-0.230	-0.259	-0.280	-0.255	-0.221
2	-0.158	-0.169	-0.191	-0.197	-0.218	-0.258	-0.198	-0.251	-0.106	-0.251	-0.255	-0.218	-0.234	-0.208
1	-0.148	-0.171	-0.208	-0.199	-0.168	-0.170	-0.185	-0.228	-0.260	-0.278	-0.250	-0.215	-0.215	-0.198

Figure VIII.-3. Output from READATA; x-direction currents

INPUT PARAMETERS
 1 SPRTS
 1 BU
 1 BU
 10 BUR
 1 BU
 2 TSCAL

THE YTD CURRENT INPUT DATA 0.0 HOURS AFTER THE BEGINNING OF THE SPILL
 AND 10 DIVISIONS IN X SPACED 0.1578-DIGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.1578-DIGREES APART.
 THE (1,1) GRID LOCATION OF THE YTD CURRENT COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.30000 DEGREES LATITUDE.
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10** -6

VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	0.256	0.256	0.256	-0.315	-0.125	-0.018	0.116	0.387	0.553	0.621	0.719	0.811	0.771	0.405
13	0.256	0.256	0.256	-0.387	-0.197	0.068	0.209	0.456	0.533	0.620	0.678	0.687	0.410	0.751
12	0.256	0.256	0.256	-0.388	-0.183	0.108	0.192	0.326	0.423	0.488	0.508	0.723	0.455	0.440
11	0.256	0.256	-0.315	-0.293	-0.189	0.185	0.178	0.261	0.377	0.416	0.487	0.420	0.576	0.459
10	0.256	0.256	0.256	0.256	-0.187	0.026	0.166	0.212	0.218	0.226	0.226	0.310	0.731	0.791
9	0.256	0.256	0.256	0.256	-0.125	-0.092	0.158	0.178	0.066	0.062	-0.022	-0.020	-0.136	-0.086
8	0.256	0.256	0.256	0.256	-0.096	-0.021	0.191	0.180	0.090	0.087	-0.018	0.019	-0.126	-0.100
7	-0.158	0.629	0.780	0.270	-0.067	-0.007	0.087	0.093	0.019	0.083	-0.089	-0.108	-0.056	-0.061
6	0.067	0.351	0.589	0.260	0.105	0.187	-0.026	-0.018	0.126	0.187	-0.076	-0.081	-0.059	-0.061
5	0.298	0.071	0.818	0.250	0.676	0.501	-0.289	-0.291	0.382	0.818	-0.108	-0.031	-0.016	-0.055
4	0.110	0.017	0.201	0.108	0.268	0.192	-0.228	-0.185	0.118	0.207	-0.080	0.087	0.067	0.072
3	-0.035	-0.080	-0.038	-0.032	-0.180	-0.120	-0.198	-0.088	-0.109	-0.010	0.025	0.115	0.158	0.188
2	-0.012	-0.008	0.015	0.017	-0.092	-0.085	-0.121	-0.089	-0.081	0.028	0.080	0.098	0.127	0.158
1	0.012	0.011	0.068	0.067	-0.081	-0.051	-0.081	-0.010	0.026	0.068	0.056	0.071	0.088	0.120

THE YTD CURRENT INPUT DATA 0.0 HOURS AFTER THE BEGINNING OF THE SPILL
 AND 10 DIVISIONS IN X SPACED 0.1578-DIGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.1578-DIGREES APART.
 THE (1,1) GRID LOCATION OF THE YTD CURRENT COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.30000 DEGREES LATITUDE.
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10** -6

VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	0.285	0.285	0.285	-0.126	-0.137	-0.030	0.122	0.175	0.381	0.610	0.728	0.801	0.758	0.588
13	0.285	0.285	0.285	-0.808	-0.209	0.052	0.197	0.488	0.522	0.612	0.567	0.875	0.788	0.718
12	0.285	0.285	0.285	-0.356	-0.195	0.093	0.180	0.318	0.411	0.456	0.486	0.711	0.681	0.678
11	0.285	0.285	-0.126	-0.303	-0.181	0.111	0.162	0.251	0.165	0.405	0.475	0.488	0.565	0.488
10	0.285	0.285	0.285	0.285	-0.159	0.018	0.155	0.201	0.206	0.218	0.218	0.299	0.218	0.281
9	0.285	0.285	0.285	0.285	-0.117	-0.103	0.187	0.162	0.058	0.050	-0.031	-0.031	-0.187	-0.108
8	0.285	0.285	0.285	0.285	-0.108	-0.032	0.182	0.128	0.078	0.015	-0.024	0.007	-0.118	-0.112
7	-0.170	0.617	0.728	0.258	-0.078	-0.019	0.076	0.081	0.007	0.071	-0.080	-0.116	-0.067	-0.071
6	0.056	0.319	0.577	0.288	0.291	0.116	-0.018	-0.010	0.118	0.175	-0.087	-0.088	-0.071	-0.075
5	0.282	0.081	0.826	0.218	0.665	0.891	-0.261	-0.211	0.310	0.802	-0.116	-0.087	-0.088	-0.067
4	0.118	0.005	0.188	0.097	0.256	0.180	-0.216	-0.156	0.108	0.191	-0.051	0.031	0.050	0.060
3	-0.087	-0.051	-0.089	-0.088	-0.152	-0.131	-0.210	-0.108	-0.121	-0.022	0.013	0.103	0.187	0.187
2	-0.021	-0.016	0.008	0.005	-0.101	-0.087	-0.112	-0.060	-0.051	0.016	0.029	0.081	0.115	0.187
1	0.0	0.018	0.057	0.055	-0.055	-0.061	-0.055	-0.022	0.018	0.052	0.088	0.061	0.081	0.108

Figure VIII.-4. Output from READATA; y-direction currents

VTID CURRENT INPUT DATA 0.0 HOURS AFTER THE BEGINNING OF THE SPILL

THE VTID CURRENT GRID HAS 10 DIVISIONS IN X SPACE 0.1578-01DFGRYS APART
AND 10 DIVISIONS IN Y SPACE 0.1578-01DFGRYS APART.

THE (1, 1) GRID LOCATION OF THE VTID CURRENT COORDINATE SYSTEM IS AT 47.00000 DEGREES LONGITUDE AND 41.10000 DEGREES LATITUDE.

ALL VALUES FOR PRESENT HAVE BEEN DIVIDED BY 10** -6

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	-0.181	-0.181	-0.181	-0.752	-0.562	-0.455	-0.301	-0.050	0.116	0.188	0.102	0.074	0.370	0.168
13	-0.181	-0.181	-0.181	-0.810	-0.630	-0.371	-0.228	0.019	0.096	0.187	0.181	0.450	0.371	0.310
12	-0.181	-0.181	-0.181	-0.782	-0.621	-0.333	-0.246	-0.112	-0.010	0.031	0.071	0.284	0.214	0.251
11	-0.181	-0.181	-0.752	-0.728	-0.606	-0.292	-0.260	-0.170	-0.060	-0.021	0.089	0.181	0.139	0.222
10	-0.181	-0.181	-0.181	-0.181	-0.585	-0.411	-0.271	-0.225	-0.219	-0.211	-0.211	-0.127	-0.204	-0.160
9	-0.181	-0.181	-0.181	-0.181	-0.562	-0.529	-0.278	-0.260	-0.371	-0.375	-0.459	-0.457	-0.579	-0.531
8	-0.181	-0.181	-0.181	-0.181	-0.533	-0.458	-0.248	-0.297	-0.161	-0.140	-0.451	-0.418	-0.569	-0.537
7	-0.595	0.192	0.301	-0.167	-0.508	-0.440	-0.350	-0.160	-0.418	-0.150	-0.346	-0.501	-0.401	-0.400
6	-0.370	-0.086	0.157	-0.177	-0.137	-0.240	-0.461	-0.455	-0.119	-0.250	-0.513	-0.520	-0.406	-0.500
5	-0.181	-0.360	0.001	-0.187	0.239	0.046	-0.446	-0.419	-0.095	-0.023	-0.101	-0.068	-0.473	-0.492
4	-0.300	-0.470	-0.231	-0.378	-0.169	-0.286	-0.441	-0.542	-0.321	-0.215	-0.477	-0.395	-0.375	-0.365
3	-0.472	-0.477	-0.475	-0.469	-0.577	-0.557	-0.615	-0.525	-0.506	-0.407	-0.412	-0.327	-0.278	-0.278
2	-0.440	-0.442	-0.422	-0.420	-0.529	-0.521	-0.558	-0.446	-0.478	-0.409	-0.197	-0.181	-0.310	-0.278
1	-0.425	-0.404	-0.369	-0.311	-0.440	-0.448	-0.440	-0.447	-0.411	-0.373	-0.181	-0.360	-0.361	-0.317

Figure VIII.-4. Output from READATA; y-direction currents

ISPT CONTROL PARAMETERS

0 BBTM
 0 BBTM
 1 BSOHR
 1 BSOH
 150 IDAT
 1 BBTM
 3.0000 DT
 10.0000 TIRRAE
 2 ISCAL
 1 BBTM
 1 BBTM
 5 BBTM
 5 BBTM
 5 BBTM
 5 BBTM
 3 BBTM
 5 BBTM
 3 BBTM
 5 BBTM
 3 BBTM
 13 BBTM
 10 BBTM
 1 BBTM
 1 BBTM
 12 BBTM
 3 BBTM
 5 BBTM
 5 BBTM
 5 BBTM
 500 BBTM
 200 BBTM
 200 BBTM
 1.0000 BBTM
 10 BBTM
 100.0000 BBTM
 0 BBTM
 1 BBTM
 1 BBTM
 1 BBTM
 10 BBTM
 11 BBTM
 10 BBTM
 15 BBTM
 0 BBTM
 9 BBTM
 0 BBTM

SPOT STRESS FOR THE SURFACE PORTION OF THE MODEL

1.33300 PORE
 1.33300 PORE
 0.05000 BEE
 0.05000 BEE
 0 BBTM
 10.00000 DEE
 10.00000 DEE
 0.00001 DEE
 0.00001 DEE
 0.00001 DEE
 0.31000 DEE
 5 INSON
 5 INSON
 3 INSON
 0 INSON
 1 BBTM
 200 BBTM
 1 BBTM
 0.50000 BBTM
 0.00000 BBTM
 0.50000 BBTM
 2.00000 BBTM
 2.00000 BBTM
 50.00000 BBTM
 0.00100 BBTM
 0.00000 BBTM
 1 BBTM
 1 BBTM
 1 BBTM
 1 BBTM
 1 BBTM
 0 BBTM
 1 BBTM
 1 BBTM

BATHYMETRY SPOT DATA 0.00 HOURS AFTER THE BEGINNING OF THE SPILL

THE BATHYMETRY GRID HAS 10 DIVISIONS IN X SPACED 0.0157 DEGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.
 THE (1,1) GRID LOCATION OF THE BATHYMETRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.35000 DEGREES LATITUDE

DEPTH VALUES IN UNITS OF METERS

J ELEMENTS	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
13	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
12	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
11	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
10	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
9	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
8	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
7	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
6	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
5	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
4	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
3	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000

COMP CELL SPOT DATA 0.00 HOURS AFTER THE BEGINNING OF THE SPILL

THE COMP CELL GRID HAS 10 DIVISIONS IN X SPACED 0.0157 DEGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.
 THE (1,1) GRID LOCATION OF THE COMP CELL COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.35000 DEGREES LATITUDE

VALUES IN UNITS OF

J ELEMENTS	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	2	2	2	2	2	2	2	2	2	2	2	2	2	2
13	2	101	101	101	101	101	101	101	101	101	101	101	101	2
12	2	101	1	1	1	1	1	1	1	1	1	1	1	2
11	2	101	1	1	1	1	1	1	1	1	1	1	1	2
10	2	101	1	1	1	1	1	1	1	1	1	1	1	2
9	2	101	1	1	1	1	1	1	1	1	1	1	1	2
8	2	101	1	1	1	1	1	1	1	1	1	1	1	2
7	2	101	1	1	1	1	1	1	1	1	1	1	1	2
6	2	101	1	1	1	1	1	1	1	1	1	1	1	2
5	2	101	1	1	1	1	1	1	1	1	1	1	1	2
4	2	101	1	1	1	1	1	1	1	1	1	1	1	2
3	2	101	1	1	1	1	1	1	1	1	1	1	1	2
2	2	101	101	101	101	101	101	101	101	101	101	101	101	2
1	2	2	2	2	2	2	2	2	2	2	2	2	2	2

SPILL CONTROL PARAMETERS 0.00 HOURS AFTER THE BEGINNING OF THE SPILL

ENVIRONMENTAL DATA READ THIS STEP: GRID CURRENT TEMPERATURE SEA STATE TIDAL HEIGHTS
 ADDITION OF SPILLSETS OR SPILL CONTROL EFFORTS THIS STEP: 1 SPILLSETS; 0 CLEANUP EFFORTS; 0 TREATMENT EFFORTS.

Figure VIII.-6. Output from Preview Run

```

WIND VEL      INPUT DATA      0.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE WIND VEL GRID HAS      1 DIVISIONS IN X SPACED      0.5000 DEGREES APART
AND      1 DIVISIONS IN Y SPACED      0.2500 DEGREES APART.
THE (1,1) GRID LOCATION OF THE WIND VEL COORDINATE SYSTEM IS AT 68.000000 DEGREES LONGITUDE AND 81.250000 DEGREES LATITUDE

      U      VALUES IN UNITS OF      M/SEC
      I ELEMENTS
Y
ELEMENTS 1
1      0.000

      V      VALUES IN UNITS OF      M/SEC
      I ELEMENTS
Y
ELEMENTS 1
1      -6.100

TEMPERATURE INPUT DATA      0.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE TEMPERATURE GRID HAS      1 DIVISIONS IN X SPACED      0.0557 DEGREES APART
AND      1 DIVISIONS IN Y SPACED      0.0157 DEGREES APART.
THE (1,1) GRID LOCATION OF THE TEMPERATURE COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 81.350000 DEGREES LATITUDE

      TEMP.      VALUES IN UNITS OF DEGREES C
      I ELEMENTS
Y
ELEMENTS 1
1      20.000

SEA STATE INPUT DATA      0.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE SEA STATE GRID HAS      1 DIVISIONS IN X SPACED      0.0157 DEGREES APART
AND      1 DIVISIONS IN Y SPACED      0.0157 DEGREES APART.
THE (1,1) GRID LOCATION OF THE SEA STATE COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 81.350000 DEGREES LATITUDE

      HEIGHT      VALUES IN UNITS OF METERS
      I ELEMENTS
Y
ELEMENTS 1
1      1.000

      PERIOD      VALUES IN UNITS OF SECONDS
      I ELEMENTS
Y
ELEMENTS 1
1      10.000

```

Figure VIII.-6. Output from Preview Run

VTID CURRENT INPUT DATA 0.00 HOURS AFTER THE BEGINNING OF THE SPELL
 THE VTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.0157 DEGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.
 THE (1,1) GRID LOCATION OF THE VTID CURRENT COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 81.366660 DEGREES LATITUDE
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10 ** -6

U VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	0.419	0.419	0.419	0.283	0.275	0.525	0.787	0.767	0.792	0.708	0.737	0.551	0.133	0.085
13	0.418	0.418	0.418	0.386	0.423	0.750	0.716	0.857	0.783	0.751	0.628	0.648	0.220	0.090
12	0.416	0.416	0.416	0.254	0.307	0.487	0.670	0.703	0.772	0.626	0.555	0.498	0.111	0.449
11	0.416	0.416	0.416	0.120	0.190	0.225	0.609	0.627	0.778	0.600	0.533	0.391	0.156	0.637
10	0.413	0.413	0.413	0.413	0.259	0.122	0.553	0.580	0.735	0.510	0.610	0.576	0.456	0.490
9	0.411	0.411	0.411	0.411	0.322	0.019	0.526	0.524	0.708	0.505	0.702	0.726	0.487	0.375
8	0.409	0.409	0.409	0.409	0.239	0.018	0.463	0.501	0.660	0.479	0.612	0.487	0.510	0.351
7	0.060	0.546	0.120	-0.102	0.157	0.053	0.386	0.429	0.617	0.413	0.471	0.484	0.390	0.328
6	0.050	0.300	0.160	-0.081	0.029	-0.060	0.197	0.174	0.224	0.183	0.280	0.409	0.125	0.136
5	0.049	0.066	0.199	-0.070	-0.100	-0.359	-0.150	-0.217	-0.551	-0.307	0.018	0.198	0.226	0.296
4	0.072	0.073	0.183	0.027	-0.071	-0.213	-0.032	-0.111	-0.318	-0.118	0.018	0.110	0.119	0.170
3	0.087	0.100	0.087	0.071	-0.041	-0.071	0.085	-0.006	-0.081	0.019	0.009	0.028	0.018	0.086
2	0.109	0.099	0.075	0.070	0.029	0.018	0.083	0.016	-0.019	0.016	0.013	0.029	0.032	0.068
1	0.123	0.096	0.083	0.068	0.098	0.097	0.082	0.019	0.007	-0.007	0.016	0.012	0.041	0.071

VTID CURRENT INPUT DATA 0.00 HOURS AFTER THE BEGINNING OF THE SPELL
 THE VTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.0157 DEGREES APART
 AND 10 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.
 THE (1,1) GRID LOCATION OF THE VTID CURRENT COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 81.366660 DEGREES LATITUDE
 ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10 ** -6

V VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	0.256	0.256	0.256	-0.315	-0.125	-0.018	0.116	0.187	0.553	0.621	0.739	0.993	0.771	0.605
13	0.256	0.256	0.256	-0.387	-0.197	0.064	0.209	0.456	0.511	0.679	0.578	0.887	0.810	0.751
12	0.256	0.256	0.256	-0.388	-0.181	0.108	0.192	0.326	0.621	0.868	0.508	0.723	0.655	0.490
11	0.256	0.256	-0.315	-0.291	-0.169	0.185	0.174	0.263	0.377	0.616	0.487	0.620	0.576	0.659
10	0.256	0.256	0.256	0.256	-0.187	0.024	0.166	0.212	0.218	0.226	0.226	0.310	0.231	0.291
9	0.256	0.256	0.256	0.256	-0.125	-0.092	0.159	0.174	0.066	0.062	-0.022	-0.020	-0.116	-0.096
8	0.256	0.256	0.256	0.256	-0.096	-0.021	0.193	0.180	0.090	0.047	-0.019	0.019	-0.126	-0.100
7	-0.150	0.629	0.780	0.270	-0.067	-0.007	0.087	0.093	0.019	0.083	-0.069	-0.186	-0.056	-0.061
6	0.067	0.351	0.589	0.260	0.105	0.187	-0.024	-0.018	0.124	0.187	-0.076	-0.083	-0.049	-0.063
5	0.294	0.071	0.418	0.250	0.676	0.501	-0.249	-0.201	0.182	0.818	-0.108	-0.031	-0.016	-0.055
4	0.130	0.017	0.201	0.109	0.248	0.192	-0.228	-0.185	0.116	0.202	-0.090	0.082	0.082	0.072
3	-0.035	-0.080	-0.018	-0.032	-0.180	-0.120	-0.198	-0.088	-0.109	-0.010	0.024	0.115	0.159	0.199
2	-0.012	-0.009	0.015	0.017	-0.097	-0.085	-0.121	-0.049	-0.041	0.028	0.080	0.098	0.127	0.159
1	0.012	0.031	0.068	0.087	-0.091	-0.051	-0.081	-0.010	0.026	0.058	0.056	0.073	0.090	0.120

Figure VIII.-6. Output from Preview Run


```

.....
REAL COEFFICIENT PARAMETERS 3.000 HOURS AFTER THE BEGINNING OF THE SPILL.
ENVIRONMENTAL DATA FOR THIS STEP: WIND          CURRENT
ADDITION OF SPILLERS OR SPILL CONTROL EFFORTS THIS STEP: 1 SPILLERS; 0 CLEANUP EFFORTS; 0 TREATMENT EFFORTS.
.....
WIND VEL          INPUT DATA          3.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE WIND VEL      GRID HAS          1 DIVISIONS IN X SPACED          0.5000 DEGREES APART
                  AND              1 DIVISIONS IN Y SPACED          0.2500 DEGREES APART.
THE (1,1) GRID LOCATION OF THE WIND VEL COORDINATE SYSTEM IS AT 64.000000 DEGREES LONGITUDE AND 81.250000 DEGREES LATITUDE

          W          VALUES IN UNITS OF          M/SEC
          I          I ELEMENTS
Y
ELEMENTS  1
1          0.000

          V          VALUES IN UNITS OF          M/SEC
          I          I ELEMENTS
Y
ELEMENTS  1
1          -5.150

UTID CURRENT INPUT DATA          3.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE UTID CURRENT GRID HAS          18 DIVISIONS IN X SPACED          0.0357 DEGREES APART
                  AND              18 DIVISIONS IN Y SPACED          0.0197 DEGREES APART.
THE (1,1) GRID LOCATION OF THE UTID CURRENT COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 81.369500 DEGREES LATITUDE
ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10 ** -6

```

```

          U          VALUES IN UNITS OF          M/S
          I          I ELEMENTS
Y
ELEMENTS  1  2  3  4  5  6  7  8  9  10  11  12  13  14
14  0.609  0.609  0.609  0.433  0.465  0.710  0.976  0.957  0.981  0.890  0.926  0.780  0.322  0.235
13  0.606  0.606  0.606  0.578  0.611  0.938  0.925  1.006  0.971  0.939  0.817  0.816  0.409  0.287
12  0.604  0.604  0.604  0.482  0.495  0.675  0.890  0.980  0.980  0.818  0.783  0.688  0.499  0.686
11  0.601  0.601  0.627  0.311  0.381  0.812  0.791  0.818  0.965  0.787  0.770  0.578  0.561  0.828
10  0.599  0.599  0.599  0.599  0.485  0.309  0.739  0.766  0.921  0.720  0.796  0.760  0.683  0.676
9   0.597  0.597  0.597  0.597  0.507  0.205  0.711  0.710  0.840  0.691  0.887  0.811  0.771  0.561
8   0.594  0.594  0.594  0.594  0.428  0.201  0.688  0.686  0.885  0.664  0.797  0.777  0.699  0.536
7   0.252  0.780  0.308  0.082  0.381  0.237  0.571  0.618  0.801  0.597  0.655  0.669  0.578  0.512
6   0.282  0.488  0.383  0.102  0.212  0.128  0.380  0.357  0.489  0.327  0.467  0.592  0.509  0.520
5   0.231  0.229  0.382  0.161  0.083  -0.176  0.033  -0.018  -0.170  -0.125  0.202  0.376  0.408  0.478
4   0.254  0.255  0.125  0.209  0.111  -0.011  0.150  0.071  -0.136  0.088  0.196  0.292  0.302  0.352
3   0.278  0.282  0.269  0.255  0.180  0.111  0.286  0.176  0.097  0.220  0.191  0.210  0.196  0.227
2   0.290  0.279  0.256  0.251  0.210  0.195  0.288  0.197  0.182  0.197  0.188  0.210  0.212  0.241
1   0.301  0.276  0.283  0.288  0.278  0.277  0.262  0.219  0.187  0.171  0.197  0.212  0.232  0.253

```

Figure VIII.-6. Output from Preview Run

VTID CURRENT INPUT DATA 1.00 HOURS AFTER THE BEGINNING OF THE SPILL

THE VTID CURRENT GRID HAS 10 DIVISIONS IN X SPACED 0.0157 DEGREES APART
AND 10 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.

THE (1,1) GRID LOCATION OF THE VTID CURRENT COORDINATE SYSTEM IS AT 67.000000 DEGREES LONGITUDE AND 41.300000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10 ** -6

Y ELEMENTS	X VALUES IN UNITS OF R/S													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	0.205	0.205	0.205	-0.326	-0.137	-0.030	0.122	0.375	0.501	0.610	0.720	0.901	0.750	0.500
13	0.205	0.205	0.205	-0.400	-0.209	0.052	0.107	0.448	0.522	0.612	0.547	0.875	0.799	0.739
12	0.205	0.205	0.205	-0.356	-0.195	0.093	0.180	0.310	0.411	0.456	0.496	0.711	0.603	0.670
11	0.205	0.205	-0.226	-0.303	-0.101	0.131	0.162	0.251	0.364	0.405	0.475	0.608	0.564	0.640
10	0.205	0.205	0.205	0.205	-0.159	0.019	0.155	0.201	0.206	0.214	0.210	0.299	0.219	0.201
9	0.205	0.205	0.205	0.205	-0.137	-0.101	0.107	0.162	0.050	0.050	-0.033	-0.031	-0.107	-0.100
8	0.205	0.205	0.205	0.205	-0.108	-0.032	0.102	0.129	0.070	0.035	-0.026	0.007	-0.130	-0.112
7	-0.170	0.617	0.720	0.750	-0.070	-0.019	0.076	0.081	0.007	0.071	-0.060	-0.116	-0.067	-0.075
6	0.056	0.339	0.577	0.748	0.293	0.136	-0.030	-0.010	0.110	0.175	-0.007	-0.040	-0.071	-0.075
5	0.202	0.061	0.026	0.210	0.665	0.091	-0.261	-0.213	0.330	0.402	-0.116	-0.082	-0.050	-0.067
4	0.110	0.005	0.100	0.097	0.256	0.100	-0.236	-0.150	0.100	0.199	-0.051	0.031	0.050	0.060
3	-0.007	-0.051	-0.009	-0.000	-0.152	-0.131	-0.210	-0.100	-0.121	-0.022	0.013	0.103	0.107	0.107
2	-0.023	-0.016	0.000	0.005	-0.103	-0.007	-0.132	-0.040	-0.051	0.016	0.020	0.003	0.114	0.107
1	0.000	0.010	0.057	0.055	-0.055	-0.063	-0.055	-0.072	0.010	0.052	0.000	0.061	0.003	0.100

SPILL 1 SPILLAGE 3.000 HOURS AFTER THE BEGINNING OF THE SPILL

SPILLAGE CREATED PRIOR TO THIS STEP

THE 1 SPILLAGE APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
IT IS CENTERED AT LONGITUDE 66.816710 AND LATITUDE 41.649400,
IS OF RADIUS 1091.99 METERS AND IS OF WEIGHT 1460.1020 METRIC TONS.

SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 1.003100 GMS/CC
INTERFACIAL TENSION 30.000000 DYNES/CM
KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.006960
PARAFFIN (C13-C22)	0.044900
CYCLOPARAFFIN (C6-C12)	0.010010
CYCLOPARAFFIN (C13-C22)	0.044907
AROMATIC (C6-C11)	0.006486
AROMATIC (C12-C18)	0.074903
HEPTHEMO-AROMATIC (C9-C25)	0.200705
RESIDUAL	0.300000

NEW SPILLAGE ADDED THIS STEP

THE 2 SPILLAGE APPEARED 3.00 HOURS AFTER THE BEGINNING OF THE SPILL
IT IS CENTERED AT LONGITUDE 66.820000 AND LATITUDE 41.649400,
IS OF RADIUS 24.00 METERS AND IS OF WEIGHT 10000.0000 METRIC TONS.

SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 0.877000 GMS/CC
INTERFACIAL TENSION 30.000000 DYNES/CM
KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.050000
PARAFFIN (C13-C22)	0.100000
CYCLOPARAFFIN (C6-C12)	0.110000
CYCLOPARAFFIN (C13-C22)	0.050000
AROMATIC (C6-C11)	0.100700
AROMATIC (C12-C18)	0.040000
HEPTHEMO-AROMATIC (C9-C25)	0.210000
RESIDUAL	0.300000

AT THIS EQUALS 3.000 HOURS THE TOTAL MASS ESTIMATED IS 146.984800 METRIC TONS
THIS RESULTS IN 0.200000 TONS PER SQUARE METER

MASS BALANCE

TOTAL MASS OF OIL SPILLED 20000.00000 METRIC TONS

LOCATION OF OIL
IN STRIPPER
OR SURFACE
IN WATER COLUMN

0 UNRECOVERED PARTICLES

AMOUNT (METRIC TONS)
20000.00000
146.984800
199.015200

PERCENT OF TOTAL
77.49
71.00
0.77

Figure VIII.-6. Output from Preview Run

```

00 BOTTOM          0 DEPOSITED PARTICLES          0.00000          0.00
00 SHORE          0.00000          0.00
REMOVAL MECHANISM
BIOLOGICALLY CONSUMED          0.00000          0.00
PHYSICALLY CLEARED UP          0.00000          0.00
LOST THRU OYPP BOUNDARY          0.00000          0.00
.....
.....
SPILL CONTROL PARAMETERS 6.000 HOURS AFTER THE BEGINNING OF THE SPILL
ENVIRONMENTAL DATA READ THIS STEP: WIND          CURRENT
ADDITION OF SPILLERS OR SPILL CONTROL EFFORTS THIS STEP: 0 SPILLERS: 0 CLEANUP EFFORTS: 0 TREATMENT EFFORTS.
.....
WIND VEL          INPUT DATA          6.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE WIND VEL          GRID RES          1 DIVISIONS IN X SPACED          0.5000 DEGREES SPARY
AND          1 DIVISIONS IN Y SPACED          0.2500 DEGREES SPARY.
THE (1,1) GRID LOCATION OF THE WIND VEL          COORDINATE SYSTEM IS AT 60.00000 DEGREES LONGITUDE AND 01.25000 DEGREES LATITUDE
.....
0          VALUES IN UNITS OF          M/SEC
I          ELEMENTS
1          2.570
.....
0          VALUES IN UNITS OF          M/SEC
I          ELEMENTS
1          0.000
.....
WIND CURRENT INPUT DATA          6.00 HOURS AFTER THE BEGINNING OF THE SPILL
THE WIND CURRENT GRID RES          10 DIVISIONS IN X SPACED          0.0357 DEGREES SPARY
AND          10 DIVISIONS IN Y SPACED          0.0157 DEGREES SPARY.
THE (1,1) GRID LOCATION OF THE WIND CURRENT COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 01.30000 DEGREES LATITUDE
ALL VALUES FOR PRESTODY HAVE BEEN DIVIDED BY 10 ** -6
.....
0          VALUES IN UNITS OF M/S
I          ELEMENTS
1          2          3          4          5          6          7          8          9          10          11          12          13          14
14          0.139          0.139          0.139          -0.037          -0.005          0.205          0.507          0.007          0.512          0.020          0.056          0.271          -0.100          -0.235
13          0.130          0.130          0.130          0.107          0.103          0.070          0.057          0.570          0.501          0.072          0.300          0.300          -0.050          -0.101
12          0.110          0.110          0.110          -0.020          0.020          0.200          0.302          0.020          0.000          0.100          0.277          0.210          0.031          0.101
11          0.137          0.137          0.301          -0.153          -0.003          -0.052          0.127          0.350          0.501          0.323          0.250          0.110          0.070          0.100
10          0.137          0.137          0.137          0.137          -0.017          -0.150          0.277          0.300          0.050          0.250          0.330          0.200          0.100          0.210
9          0.130          0.130          0.130          0.130          0.007          -0.250          0.251          0.250          0.020          0.210          0.027          0.051          0.312          0.100
8          0.130          0.130          -0.110          0.110          -0.015          -0.250          0.100          0.227          0.307          0.205          0.310          0.111          0.200          0.077
7          -0.205          -0.203          -0.151          -0.015          -0.110          -0.220          0.110          0.157          0.300          0.100          0.100          0.212          0.121          0.055
6          -0.211          -0.020          -0.112          -0.351          -0.201          -0.311          -0.075          -0.000          -0.000          -0.120          0.012          0.117          0.050          0.000
5          -0.222          -0.220          -0.071          -0.201          -0.370          -0.020          -0.000          -0.000          -0.020          -0.570          -0.252          -0.077          -0.005          0.025
4          -0.190          -0.190          -0.127          -0.202          -0.301          -0.003          -0.302          -0.101          -0.500          -0.001          -0.255          -0.100          -0.100          -0.000
3          -0.172          -0.100          -0.101          -0.190          -0.110          -0.310          -0.100          -0.275          -0.351          -0.210          -0.250          -0.200          -0.255          -0.271
2          -0.150          -0.100          -0.101          -0.107          -0.210          -0.200          -0.100          -0.251          -0.100          -0.251          -0.210          -0.210          -0.210          -0.200
1          -0.100          -0.171          -0.200          -0.100          -0.100          -0.170          -0.100          -0.220          -0.200          -0.270          -0.250          -0.215          -0.215          -0.100

```

Figure VIII.-6. Output from Preview Run

VTID CURRENT INPUT DATA 6.00 HOURS AFTER THE BEGINNING OF THE SPILL

THE VTID CURRENT GRID HAS 16 DIVISIONS IN X SPACED 0.0157 DEGREES APART
AND 16 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.

THE (1,1) GRID LOCATION OF THE VTID CURRENT COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.30000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT HAVE BEEN DIVIDED BY 10 ** -6

V VALUES IN UNITS OF M/S

Y ELEMENTS	X ELEMENTS															
	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16
16	-0.181	-0.181	-0.181	-0.152	-0.562	-0.455	-0.303	-0.050	0.116	0.180	0.302	0.476	0.310	0.168		
15	-0.181	-0.181	-0.181	-0.438	-0.634	-0.373	-0.228	0.019	0.096	0.187	0.181	0.450	0.373	0.310		
12	-0.181	-0.181	-0.181	-0.182	-0.621	-0.333	-0.246	-0.112	-0.018	0.031	0.071	0.246	0.210	0.253		
11	-0.181	-0.181	-0.181	-0.181	-0.606	-0.292	-0.260	-0.170	-0.060	-0.021	0.049	0.183	0.139	0.222		
10	-0.181	-0.181	-0.181	-0.181	-0.585	-0.411	-0.271	-0.225	-0.210	-0.211	-0.211	-0.127	-0.208	-0.180		
9	-0.181	-0.181	-0.181	-0.181	-0.562	-0.529	-0.278	-0.260	-0.371	-0.375	-0.459	-0.457	-0.573	-0.533		
8	-0.181	-0.181	-0.181	-0.181	-0.533	-0.458	-0.240	-0.297	-0.347	-0.340	-0.451	-0.418	-0.563	-0.517		
7	-0.595	0.192	0.303	-0.167	-0.508	-0.400	-0.350	-0.300	-0.418	-0.350	-0.400	-0.501	-0.493	-0.440		
6	-0.370	-0.086	0.192	-0.177	-0.137	-0.290	-0.463	-0.455	-0.311	-0.256	-0.513	-0.520	-0.446	-0.500		
5	-0.183	-0.369	0.001	-0.187	0.239	0.066	-0.686	-0.639	-0.095	-0.023	-0.581	-0.468	-0.473	-0.492		
4	-0.308	-0.420	-0.237	-0.228	-0.169	-0.246	-0.661	-0.582	-0.321	-0.215	-0.477	-0.395	-0.375	-0.365		
3	-0.472	-0.477	-0.475	-0.469	-0.577	-0.557	-0.635	-0.525	-0.586	-0.487	-0.442	-0.322	-0.378	-0.278		
2	-0.449	-0.442	-0.422	-0.420	-0.529	-0.523	-0.558	-0.486	-0.478	-0.409	-0.397	-0.383	-0.310	-0.278		
1	-0.425	-0.406	-0.369	-0.371	-0.440	-0.488	-0.480	-0.487	-0.411	-0.371	-0.381	-0.360	-0.303	-0.317		

SPILLERS APPEARING 6.000 HOURS AFTER THE BEGINNING OF THE SPILL

SPILLERS CREATED PRIOR TO THIS STEP

THE 1 SPILLER APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
IT IS CENTERED AT LONGITUDE 66.811840 AND LATITUDE 41.632010,
IS OF RADIUS 1300.71 METERS AND IS OF HEIGHT 7817.1550 METRIC TONS.

SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 1.000056 GRAMS/CC
INTERFACIAL TENSION 30.000000 DYNES/CM
KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.002223
PARAFFIN (C13-C22)	0.099988
CYCLOPARAFFIN (C6-C12)	0.007175
CYCLOPARAFFIN (C13-C22)	0.000000
AROMATIC (C6-C11)	0.000795
AROMATIC (C12-C18)	0.079409
HETERO-AROMATIC (C9-C25)	0.209660
RESIDUAL	0.300000

THE 2 SPILLER APPEARED 3.00 HOURS AFTER THE BEGINNING OF THE SPILL
IT IS CENTERED AT LONGITUDE 66.810640 AND LATITUDE 41.651060,
IS OF RADIUS 1094.71 METERS AND IS OF HEIGHT 7999.4010 METRIC TONS.

SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 0.995209 GRAMS/CC
INTERFACIAL TENSION 30.000000 DYNES/CM
KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.013924
PARAFFIN (C13-C22)	0.099998
CYCLOPARAFFIN (C6-C12)	0.016179
CYCLOPARAFFIN (C13-C22)	0.000000
AROMATIC (C6-C11)	0.011710
AROMATIC (C12-C18)	0.079461
HETERO-AROMATIC (C9-C25)	0.209660
RESIDUAL	0.300000

AT TIME EQUALS 6.000000 HOURS THE TOTAL MASS REMAINING IS 161.054100 METRIC TONS
THIS RESULTS IN 0.122117 TONS PER SQUARE SPREAD OUT OVER 400 PARTICLES

MASS BALANCE

TOTAL MASS OF OIL SPILLED 20000.00000 METRIC TONS

LOCATION OF OIL	AMOUNT (METRIC TONS)	PERCENT OF TOTAL
IN ATMOSPHERE	8478.71800	21.39
ON SURFACE	15140.18000	75.40
IN WATER COLUMN	161.05410	0.81
ON BOTTOM	0.00000	0.00
ON SHORE	0.00000	0.00
REMOVAL MECHANISMS		

Figure VIII.-6. Output from Preview Run

```

      BIOLOGICALLY CONSUMED          0.00000          0.00
      PHYSICALLY CLEARED OF         0.00000          0.00
      LOST THRU OPRR MANDATORY      0 LOST PARTICLES 0.00000          0.00
.....
      SPILL CONTROL PARAMETERS ..... 9.000 HOURS AFTER THE BEGINNING OF THE SPILL
.....
      ENVIRONMENTAL DATA READ THIS STEP:          CORR
      ADDITION OF SPILLERS OR SPILL CONTROL EFFORTS THIS STEP: 0 SPILLERS; 0 CLEANUP EFFORTS; 0 TREATMENT EFFORTS.
.....
      RELEASE SPILLERS ..... 9.000 HOURS AFTER THE BEGINNING OF THE SPILL
      SPILLERS CREATED PRIOR TO THIS STEP
      THE 1 SPILLER APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
      IT IS CENTERED AT LONGITUDE 64.799710 AND LATITUDE 41.627160,
      IS OF RADIUS 1000.00 METERS AND IS OF WEIGHT 7378.4000 METRIC TONS.
      SOME PROPERTIES OF THE SPILLED OIL ARE:
      DENSITY 1.010876 GIBBS/CC
      INTERFACIAL TENSION 30.000000 DYNES/CM
      KINEMATIC VISCOSITY 1.000000 CENTISTOKES
      BY WEIGHT THE OIL FRACTIONS ARE:
      PARAFFIN (C6-C12) 0.004520
      PARAFFIN (C13-C22) 0.000002
      CYCLOPARAFFIN (C6-C12) 0.000219
      CYCLOPARAFFIN (C13-C22) 0.000005
      AROMATIC (C6-C11) 0.000040
      AROMATIC (C12-C18) 0.074498
      NAPHTHENO-AROMATIC (C9-C25) 0.209618
      RESIDUAL 0.100000
      THE 2 SPILLER APPEARED 3.00 HOURS AFTER THE BEGINNING OF THE SPILL
      IT IS CENTERED AT LONGITUDE 64.802730 AND LATITUDE 41.644110,
      IS OF RADIUS 1301.01 METERS AND IS OF WEIGHT 7781.7070 METRIC TONS.
      SOME PROPERTIES OF THE SPILLED OIL ARE:
      DENSITY 1.000205 GIBBS/CC
      INTERFACIAL TENSION 30.000000 DYNES/CM
      KINEMATIC VISCOSITY 1.000000 CENTISTOKES
      BY WEIGHT THE OIL FRACTIONS ARE:
      PARAFFIN (C6-C12) 0.000060
      PARAFFIN (C13-C22) 0.000002
      CYCLOPARAFFIN (C6-C12) 0.025888
      CYCLOPARAFFIN (C13-C22) 0.000000
      AROMATIC (C6-C11) 0.001512
      AROMATIC (C12-C18) 0.019451
      NAPHTHENO-AROMATIC (C9-C25) 0.209818
      RESIDUAL 0.100000
.....
      AT TIME EQUALS 9.000000HOURS THE TOTAL MASS REMAINDER IS 175.841500METRIC TONS
      THIS RESULTS IN 0.151700TONS PER SQUARE METER SPREAD OUT OVER 500PARTICLES
.....
      MASS BALANCE
      TOTAL MASS OF OIL SPILLED 20000.00000 METRIC TONS
      LOCATION OF OIL          AMOUNT (METRIC TONS)          PERCENT OF TOTAL
      IN ATMOSPHERE          4816.22200          24.1%
      ON SURFACE          14883.77800          74.9%
      IN WATER COLUMN      0 HADDER PARTICLES          0.0%
      ON BOTTOM          0 DEPOSITED PARTICLES          0.0%
      ON SHORE          0.00000          0.0%
      REMOVAL MECHANISMS
      BIOLOGICALLY CONSUMED          0.00000          0.0%
      PHYSICALLY CLEARED OF         0.00000          0.0%
      LOST THRU OPRR MANDATORY      0 LOST PARTICLES          0.0%
.....

```

Figure VIII.-6. Output from Preview Run

.....
SPILL CONTROL PARAMETERS 12,000 HOURS AFTER THE BEGINNING OF THE SPILL

ENVIRONMENTAL DATA READ THIS STEP: NONE
 ADDITION OF SPILLETTS OR SPILL CONTROL EFFORTS THIS STEP: 0 SPILLETTS; 1 CLEANUP EFFORTS; 0 TREATMENT EFFORTS.

PHYSICAL CLEANUP REPORTS IN PROGRESS 12,00000 HOURS AFTER THE BEGINNING OF THIS SPILL

FOR CLEANUP EFFORTS THIS TIME STEP

THE 1 CLEANUP EFFORT CURRENTLY UNDERWAY IS CENTERED AT LONGITUDE 66.770000 AND LATITUDE 41.619990
 THE RADIUS OF COVERAGE OF THIS EFFORT IS 10000.000 METERS
 THE RAZORH RATE OF RECOVERY IS 100.000000 TONS/HOUR WITH AN EFFICIENCY OF 50.000000
 THIS CLEANUP STARTS 12.000000 HOURS AFTER THE BEGINNING OF THE SPILL AND LASTS 6.000000 HOURS

EXISTING SPILLETTS 12,000 HOURS AFTER THE BEGINNING OF THE SPILL

SPILLETTS CREATED PRIOR TO THIS STEP

THE 1 SPILLET APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.787010 AND LATITUDE 41.621790,
 IS OF RADIUS 1894.98 METERS AND IS OF WEIGHT 7199.8710 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:

DEENSITY 1.011191 GBARS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES
 BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.001065
PARAFFIN (C13-C22)	0.099930
CYCLOPARAFFIN (C6-C12)	0.001804
CYCLOPARAFFIN (C13-C22)	0.084905
AROMATIC (C6-C11)	0.000286
AROMATIC (C12-C18)	0.079887
PARAFFINO-AROMATIC (C9-C25)	0.209817
RESIDUAL	0.100000

THE 2 SPILLET APPEARED 3.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.790710 AND LATITUDE 41.644280,
 IS OF RADIUS 1897.68 METERS AND IS OF WEIGHT 7437.9880 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:

DEENSITY 1.003819 GBARS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES
 BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.006669
PARAFFIN (C13-C22)	0.099930
CYCLOPARAFFIN (C6-C12)	0.018873
CYCLOPARAFFIN (C13-C22)	0.084905
AROMATIC (C6-C11)	0.000178
AROMATIC (C12-C18)	0.079980
PARAFFINO-AROMATIC (C9-C25)	0.209776
RESIDUAL	0.100000

.....
 DURING THE TIME STEP WHICH BEGINS AT 12.000000 HOURS 300.000000 TONS OF OIL WERE PHYSICALLY REMOVED FROM THE 1 SPILLET
 DURING THE TIME STEP WHICH BEGINS AT 12.000000 HOURS 100.000000 TONS OF OIL WERE PHYSICALLY REMOVED FROM THE 2 SPILLET
 AT THIS POINTS THE TOTAL MASS WITHAIND IS 189.117100METRIC TONS
 THIS RESULTS IN 0.3782 TONS PER DROPLET SPREAD ORY OVER 500PARTICLES

MASS BALANCE

TOTAL MASS OF OIL SPILLED 20000.00000 METRIC TONS

LOCATION OF OIL	AMOUNT (METRIC TONS)	PERCENT OF TOTAL
IN ATMOSPHERE	8917.10000	24.49
ON SURFACE	14271.51000	71.17
IN WATER COLUMN	189.11710	0.94
ON BOTTOM	0.00000	0.00
ON SHORE	0.00000	0.00
REMOVAL MECHANISMS		
BIOLOGICALLY CONSUMED	0.00000	0.00
PHYSICALLY CLEANED UP	600.00000	3.00
LOST THROUGH RECOVERY	0.00000	0.00

.....

Figure VIII.-6. Output from Preview Run

.....
SPILL CONTROL PARAMETERS 15,000 HOURS AFTER THE BEGINNING OF THE SPILL.
 ENVIRONMENTAL DATA FROM THIS STEP: NONE
 ADDITION OF SPILLERS OR SPILL CONTROL EFFORTS THIS STEP: 0 SPILLERS; 0 CLEARUP EFFORTS; 0 TREATMENT EFFORTS.

PHYSICAL CLEANUP EFFORTS IN PROGRESS 15,0000 HOURS AFTER THE BEGINNING OF THIS STEP
 CONTINUING SPILL CLEARUP EFFORTS THIS STEP

THE 1 CLEARUP EFFORT CURRENTLY UNDERWAY IS CENTERED AT LONGITUDE 66.770000 AND LATITUDE 61.610000
 THE RADIUS OF COVERAGE OF THIS EFFORT IS 10000.000 METERS
 THE RATING RATE OF RECORD IS 100.000000 TONS/HOUR WITH AN EFFICIENCY OF 50.000000
 THIS CLEARUP STARTS 12.000000 HOURS AFTER THE BEGINNING OF THE SPILL AND LASTS 6.000000 HOURS

ELICTION SPILLERS 15,000 HOURS AFTER THE BEGINNING OF THE SPILL
 SPILLERS CREATED PRIOR TO THIS STEP

THE 1 SPILLER APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.770320 AND LATITUDE 61.620270,
 IS OF RADIUS 1684.73 METERS AND IS OF WEIGHT 7290.4170 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 1.011690 GRAMS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.800722
PARAFFIN (C13-C22)	0.000000
CYCLOPARAFFIN (C6-C12)	0.002157
CYCLOPARAFFIN (C13-C22)	0.000000
AROMATIC (C6-C11)	0.000118
AROMATIC (C12-C16)	0.074077
SEMIAROMATIC (C6-C25)	0.200517
SPERMAL	0.300000

THE 2 SPILLER APPEARED 1.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.770010 AND LATITUDE 61.640010,
 IS OF RADIUS 1684.63 METERS AND IS OF WEIGHT 7290.4170 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 1.006613 GRAMS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.800000
PARAFFIN (C13-C22)	0.000000
CYCLOPARAFFIN (C6-C12)	0.010000
CYCLOPARAFFIN (C13-C22)	0.000000
AROMATIC (C6-C11)	0.002111
AROMATIC (C12-C16)	0.074020
SEMIAROMATIC (C6-C25)	0.200715
SPERMAL	0.300000

.....
 DURING THE TIME STEP WHICH BEGAN AT 15.000000 HOURS 300.000000 TONS OF OIL WERE PHYSICALLY REMOVED FROM THE 1 SPILLER
 DURING THE TIME STEP WHICH BEGAN AT 15.000000 HOURS 100.000000 TONS OF OIL WERE PHYSICALLY REMOVED FROM THE 2 SPILLER
 AT TIME EQUALS 15.000000 THE TOTAL MASS ESTIMATED IS 200.921000 METRIC TONS
 THIS RESULTS IN 0.401800 TONS PER DROPLET SPREAD NOT OVER 500 PARTICLES

MASS BALANCE

LOCATION OF OIL	AMOUNT (METRIC TONS)	PERCENT OF TOTAL
TOTAL MASS OF OIL SPILLED	20000.00000	100.00000
IN ATMOSPHERE	4003.20100	20.02
ON SURFACE	13595.02000	67.98
IN WATER COLUMN	0.00000	0.00
ON BOTTOM	0.00000	0.00
ON SHORE	0.00000	0.00
REMOVED MECHANICALLY	0.00000	0.00
BIOLOGICALLY CONSUMED	1200.00000	6.00
PHYSICALLY CLEARED UP	0.00000	0.00
LOST THROUGH FOUHRAST	0.00000	0.00

.....
 CODE USAGE OBJECT CODE= 160064 BYTES, AREA= 100416 BYTES, TOTAL AREA AVAILABLE= 505846 BYTES
 DIAGNOSTICS NUMBER OF RECORDS= 0, NUMBER OF RECORDS= 11, NUMBER OF EXTENSIONS= 2
 BAPPIV - JUL 1973 FILE 12.52.50 THURSDAY 22 MAY 80
 /END

Figure VIII.-6. Output from Preview Run

INPUT CONTROL PARAMETERS INPUT STRIP FOR THE SUBSEQUENT POSITION OF THE MODEL

PARAMETERS INPUT DATA 0.00 10000 APPR FOR APPROXIMATE OF THE SPILL

0	WSPR	1.11100	WSPR	THE PARAMETER GRID HAS 10 DIVISIONS IN X SPACE	0.0157 DEGREE APART
1	WSPR	1.11100	WSPR	AND 10 DIVISIONS IN Y SPACE	0.0157 DEGREE APART.
0	WSPR	0.05000	WSPR	THE (1,1) GRID LOCATION OF THE PARAMETER COORDINATE SYSTEM IS AT 67.00000 DEGREE EASTING AND 61.15000 DEGREE LATITUDE	
150	WSPR	0.05000	WSPR		
1	WSPR	0	WSPR		
1.00000	WSPR	10.00000	WSPR		
14.00000	WSPR	10.00000	WSPR		
2	WSPR	0.00001	WSPR		
1	WSPR	0.00001	WSPR		
1	WSPR	0.00001	WSPR		
5	WSPR	0.33000	WSPR		
5	WSPR	5	WSPR		
6	WSPR	4	WSPR		
5	WSPR	1	WSPR		
3	WSPR	0	WSPR		
5	WSPR	1	WSPR		
1	WSPR	200	WSPR		
5	WSPR	1	WSPR		
3	WSPR	0.50000	WSPR		
5	WSPR	8.00000	WSPR		
3	WSPR	0.50000	WSPR		
13	WSPR	2.00000	WSPR		
16	WSPR	2.00000	WSPR		
1	WSPR	50.00000	WSPR		
1	WSPR	0.00100	WSPR		
12	WSPR	0.00000	WSPR		
3	WSPR	1	WSPR		
5	WSPR	1	WSPR		
5	WSPR	1	WSPR		
5	WSPR	1	WSPR		
5	WSPR	1	WSPR		
500	WSPR	1	WSPR		
200	WSPR	0	WSPR		
200	WSPR	1	WSPR		
1.00000	WSPR	1	WSPR		
10	WSPR	1	WSPR		
100.00000	WSPR	1	WSPR		
0	WSPR	1	WSPR		
1	WSPR	1	WSPR		
1	WSPR	1	WSPR		
10	WSPR	1	WSPR		
11	WSPR	1	WSPR		
10	WSPR	1	WSPR		
15	WSPR	1	WSPR		
8	WSPR	1	WSPR		
9	WSPR	1	WSPR		
0	WSPR	1	WSPR		

APPR VALUES IN UNITS OF METERS

Y	X	X													
		1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
11	1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
12	1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
11	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
10	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
9	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
8	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
7	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
6	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
5	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
4	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
3	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
2	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
1	2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
2	1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000

COMP CPLL INPUT DATA 0.00 10000 APPR FOR APPROXIMATE OF THE SPILL

THE COMP CPLL GRID HAS 10 DIVISIONS IN X SPACE AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREE APART 0.0157 DEGREE APART.

THE (1,1) GRID LOCATION OF THE COMP CPLL COORDINATE SYSTEM IS AT 67.00000 DEGREE EASTING AND 61.15000 DEGREE LATITUDE

VALUES IN UNITS OF

Y	X	X													
		1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	1	2	2	2	2	2	2	2	2	2	2	2	2	2	2
11	1	2	101	101	101	101	101	101	101	101	101	101	101	101	2
12	1	2	101	9	1	1	1	1	1	1	1	1	1	1	2
11	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
10	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
9	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
8	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
7	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
6	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
5	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
4	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
3	2	2	101	9	1	1	1	1	1	1	1	1	1	1	2
2	2	2	101	101	101	101	101	101	101	101	101	101	101	101	2
1	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2

Figure VIII.-7. Output from Main Simulation

```

.....
      SPILL CONTROL PARAMETERS.....0.000 HOURS AFTER THE BEGINNING OF THE SPILL.
PROVISIONAL DATA FOR THIS STEP: WIND          CURRENT          TEMPERATURE          SEA STATE          FINAL MOTION
ANNOTATION OF SPILLS OR SPILL CONTROL REPORTS THIS STEP:  1 SPILLS:      1 CLEANUP SPILLS:  0 POLYMER SPILLS
.....

      WIND VFL          INPUT DATA          0.00 HOURS AFTER THE BEGINNING OF THE SPILL
FOR WIND VFL          GRID HAS          1 DIVISIONS IN X SPACE          0.5000 DEGREES APART
                      AND          1 DIVISIONS IN Y SPACE          0.2500 DEGREES APART.
THE (1,1) GRID LOCATION OF THE WIND VFL          COORDINATE SYSTEM IS AT 65.00000 DEGREES LONGITUDE AND 81.25000 DEGREES LATITUDE

          0          VALUES IN UNITS OF          M/SEC
          Y          Y ELEMENTS
ELEMENTS          1
1          0.000

          Y          VALUES IN UNITS OF          M/SEC
          Y          Y ELEMENTS
ELEMENTS          1
1          -0.100

0

      TEMPERATURE INPUT DATA          0.00 HOURS AFTER THE BEGINNING OF THE SPILL
FOR TEMPERATURE GRID HAS          1 DIVISIONS IN X SPACE          0.0157 DEGREES APART
                      AND          1 DIVISIONS IN Y SPACE          0.0157 DEGREES APART.
THE (1,1) GRID LOCATION OF THE TEMPERATURE          COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 81.25000 DEGREES LATITUDE

          TEMP.          VALUES IN UNITS OF          DEGREES C
          Y          Y ELEMENTS
ELEMENTS          1
1          20.000

      SEA STATE INPUT DATA          0.00 HOURS AFTER THE BEGINNING OF THE SPILL
FOR SEA STATE          GRID HAS          1 DIVISIONS IN X SPACE          0.0157 DEGREES APART
                      AND          1 DIVISIONS IN Y SPACE          0.0157 DEGREES APART.
THE (1,1) GRID LOCATION OF THE SEA STATE          COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 81.25000 DEGREES LATITUDE

          STATE          VALUES IN UNITS OF          STATES
          Y          Y ELEMENTS
ELEMENTS          1
1          1.000

          PERIOD          VALUES IN UNITS OF          SECONDS
          Y          Y ELEMENTS
ELEMENTS          1
1          10.000

```

Figure VIII.-7. Output from Main Simulation

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

Y ELEMENTS	X										Z ELEMENTS				
	1	2	3	4	5	6	7	8	9	10	1	2	3	4	5
10	0.810	0.810	0.810	0.761	0.774	0.525	0.787	0.747	0.702	0.708	0.737	0.541	0.311	0.008	
11	0.810	0.810	0.810	0.748	0.827	0.740	0.716	0.857	0.783	0.751	0.828	0.848	0.770	0.098	
12	0.810	0.810	0.810	0.720	0.707	0.887	0.870	0.783	0.772	1.826	0.555	0.898	0.341	0.859	
11	0.810	0.810	0.800	0.770	0.748	0.275	0.408	0.627	0.778	0.510	1.411	0.391	0.196	0.617	
10	0.813	0.813	0.813	0.813	0.754	0.122	0.553	0.380	0.715	0.310	0.810	3.378	0.858	0.800	
9	0.811	0.811	0.811	0.811	0.722	0.814	0.528	0.528	0.708	3.505	0.702	0.778	0.487	0.315	
8	0.809	0.809	0.809	0.809	0.719	0.818	0.843	0.501	0.660	0.178	1.512	1.587	0.518	0.151	
7	0.808	0.808	0.808	-0.182	0.147	0.053	0.186	0.829	0.817	0.313	0.871	0.880	0.398	0.128	
6	0.808	0.808	0.808	-0.081	0.029	-0.040	0.187	0.178	0.725	0.111	1.288	0.809	0.325	0.116	
5	0.809	0.808	0.809	-0.020	-0.100	-0.158	-0.150	-0.211	-0.553	-0.137	0.819	1.288	0.728	0.298	
4	0.812	0.813	0.813	0.827	-0.071	-0.211	-0.032	-0.111	-0.318	-0.138	0.818	0.118	0.118	0.118	
3	0.807	0.808	0.807	0.813	-0.081	-0.071	0.085	-0.086	-0.081	0.818	1.009	0.828	0.818	0.888	
2	0.808	0.809	0.815	0.870	0.829	0.818	0.883	0.818	-0.018	0.818	3.211	0.828	0.812	0.868	
1	0.123	0.096	0.081	0.068	0.098	0.087	0.082	-0.018	0.087	-0.887	3.218	3.212	0.858	0.878	

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

WTD CHERRY EMBY DATA 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.00

THE WTD CHERRY DATA HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPACE
AND 10 DIVISIONS IN Y SPACE 0.0157 DEGREES SPACE

THE (1,1) GRID LOCATION OF THE WTD CHERRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR DISTURBANCE HAVE BEEN DIVIDED BY 10 ** -6

Y ELEMENTS	X										Z ELEMENTS				
	1	2	3	4	5	6	7	8	9	10	1	2	3	4	5
10	0.248	0.248	0.248	-0.115	-0.125	-0.018	0.118	0.387	0.553	3.821	3.718	1.815	0.321	3.498	
11	0.248	0.248	0.248	-0.187	-0.187	0.068	0.709	0.854	0.511	0.620	0.578	0.887	0.810	0.151	
12	0.248	0.248	0.248	-0.188	-0.183	0.108	0.182	0.328	0.827	0.558	0.509	3.728	0.845	0.688	
11	0.248	0.248	-0.115	-0.291	-0.168	0.185	0.178	0.261	0.327	0.816	0.887	0.678	0.176	0.648	
10	0.248	0.248	0.248	0.248	-0.187	0.028	0.168	0.212	0.718	0.225	0.722	0.118	0.211	3.293	
9	0.248	0.248	0.248	0.248	-0.125	-0.082	0.158	0.178	0.845	3.312	-3.322	-0.320	-0.118	-0.098	
8	0.248	0.248	0.248	0.248	-0.084	-0.021	0.183	0.188	0.888	0.887	-0.818	-0.818	-0.128	-0.108	
7	-0.158	0.829	0.788	0.270	-0.087	-0.087	0.087	-0.081	0.818	3.211	-3.088	-0.188	-0.088	-3.081	
6	0.087	0.351	0.588	0.288	0.185	0.187	-0.028	-0.018	0.128	3.147	-0.878	-0.881	-0.889	-0.881	
5	0.298	0.871	0.878	0.248	0.678	0.583	-0.288	-0.281	0.382	3.818	-0.188	-0.811	-0.818	-0.885	
4	0.118	0.817	-0.281	0.188	0.248	0.182	-0.228	-0.185	0.115	0.282	-0.888	0.882	0.887	0.872	
3	-0.035	-0.088	-0.818	-0.012	-0.188	-0.128	-0.188	-0.088	-0.188	-0.188	-0.818	0.828	0.118	0.188	
2	-0.012	-0.088	0.815	0.817	-0.082	-0.085	-0.121	-0.089	-0.889	3.828	0.818	0.298	0.127	0.118	
1	0.012	0.011	0.088	0.087	-0.081	-0.081	-0.081	-0.818	0.825	3.358	0.555	1.871	0.088	0.128	

Figure VIII.-7. Output from Main Simulation

THE TOP LEVEL DATA ARE IN DIVISIONS IN X SPACES 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IS OF PAGES 25, 26 AFTER AND IS OF SPACES 10000.0000 AFTER THE
 THE (1,1) GRID LOCATION OF THE TOP LEVEL COORDINATE SYSTEM IS AT 61.000000 DEGREES LONGITUDE AND 01.350000 DEGREES LATITUDE

VALUES IN UNITS OF OBTAIN

Y ELAPSE	1	2	3	4	5	6	7	8	9	10	11	12	13	14
16	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
15	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
14	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
13	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
12	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
11	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
10	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
9	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
8	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
7	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
6	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
5	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
4	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
3	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
2	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000
1	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000

CONTINUED SPILLS: 0.00 HOURS AFTER THE BEGINNING OF THE SPILL

THE SPILLER APPLIED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IS CENTERED AT LONGITUDE 64.000000 AND LATITUDE 01.660000
 IS OF PAGES 25, 26 AFTER AND IS OF SPACES 10000.0000 AFTER THE
 SOME PROPERTIES OF THE SPILLER OIL ARE:
 DENSITY 0.870000 GRAMS/CC
 INTERFACIAL TENSION 10.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES
 BY WEIGHT THE OIL CONTAINS ARE:
 PARAFFIN (24-32) 0.053770
 PARAFFIN (33-37) 0.100370
 CYCLOPARAFFIN (34-42) 0.140333
 CYCLOPARAFFIN (43-52) 0.053770
 AROMATIC (24-33) 0.133333
 AROMATIC (34-42) 0.000370
 NAPHTHENE-AROMATIC (43-52) 0.213333
 RESIDUAL 0.100370

CLOSURE GRID DEFINITION AND PARTICLE LOCATION STATISTICS
 ORIGIN OF FLOATING GRID IS AT (0.0000, 0.0000) IN DEGREES WITH DEGREE IN THE UNITS OF THE PLETH UPPER GRID
 THE GRID ORIGIN COORDINATE IN THE PLETHORIC SYSTEM IS (0.000000, 0.000000) IN X AND (0.000000, 0.000000) IN Y
 THE GRID COORDINATE IN THE PLETHORIC SYSTEM IS (0.000000, 0.000000) IN X AND (0.000000, 0.000000) IN Y
 THE APPROX VALUE OF X, Y AND Z ARE 0.000000, 0.000000, 0.000000
 THE STANDARD DEVIATIONS ARE 0.000000, 0.000000, 0.000000
 HORIZONTAL X-Y SCALE DEPENDENT DIFFERENCE (DIFF) 0.000000, 0.000000
 XERR= 0.000000, YERR= 0.000000, ZERR= 0.000000, XERR= 0.000000, YERR= 0.000000, ZERR= 0.000000

Figure VIII.-7. Output from Main Simulation

3. SUBSONIC VELOCITIES AND MULTIPLIER BY 10000

U VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.065	0.065	0.065
0.2	0.068	0.068	0.067
0.2	0.068	0.068	0.068
0.2	0.070	0.070	0.070
0.2	0.071	0.072	0.072

U VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.064	0.064	0.065
0.2	0.068	0.068	0.067
0.2	0.068	0.068	0.068
0.2	0.070	0.070	0.070
0.2	0.071	0.072	0.072

U VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.064	0.064	0.065
0.2	0.068	0.068	0.067
0.2	0.068	0.068	0.068
0.2	0.070	0.070	0.070
0.2	0.071	0.072	0.072

V VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	-0.076	-0.076	-0.076
0.2	-0.079	-0.079	-0.079
0.2	-0.079	-0.079	-0.079
0.2	-0.071	-0.073	-0.071
0.2	-0.072	-0.072	-0.072

V VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	-0.074	-0.074	-0.076
0.2	-0.074	-0.074	-0.074
0.2	-0.078	-0.078	-0.078
0.2	-0.071	-0.071	-0.073
0.2	-0.072	-0.072	-0.072

V VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	-0.074	-0.074	-0.076
0.2	-0.074	-0.074	-0.074
0.2	-0.078	-0.078	-0.078
0.2	-0.071	-0.073	-0.071
0.2	-0.072	-0.072	-0.072

W VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000

W VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.000	0.000	0.000

U VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000

U VELOCITY FIELD	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000
0.2	0.000	0.000	0.000

VELOCITY GRID DEFINITION AND PARTICLE LOCATION STATISTICS

NUMBER OF PLASTIC GRID IS 27 0.2162 0.1567 IN ACCEPTS WITH SPACED TO THE SPACES OF THE STPP NUMBER WITH
 THE GRID SPACED TO THE PLASTIC GRID IS 0.000156 SPACES IN X AND 0.000156 SPACES IN Y
 THE GRID SPACED TO THE STPP NUMBER IS 0.016 SPACES IN X AND 0.016 SPACES IN Y
 THE STPP NUMBER VALUES OF X, Y AND Z ARE 0.000271 0.000271 0.216225
 THE STANDARD DEVIATIONS ARE 0.000044 0.000044 0.161958

CONCENTRATION IN NO OF OIL PER ML OF WATER	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000

CONCENTRATION IN NO OF OIL PER ML OF WATER	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000

CONCENTRATION IN NO OF OIL PER ML OF WATER	STPP NUMBER	Q	TWR
0.16	0.16	0.16	0.16
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000
0.22	0.00000	0.00000	0.00000

Figure VIII.-7. Output from Main Simulation

PARTICLE POSITIONS IN BOX Y IN THE FLOWING SYSTEM IN SPACES X IN SPACES
 PARTICLE PARALLELS AT TIME 0.00

N	PARTICLE POSITION FLOWING SYSTEM			PARTICLE POSITION FIELD SYSTEM			PARTICLE PARALLELS			WGT
	X	Y	Z	X	Y	Z	SPACED	SPACED	SPACED	
1	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
2	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	3.0000	1.000
3	0.0001	0.0002	0.8037	0.216	0.354	0.8137	0.0510	0.8770	0.0000	1.000
4	0.0001	0.0001	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
5	0.0002	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
6	0.0002	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
7	0.0001	0.0002	0.8150	0.216	0.354	0.8150	3.0513	0.8770	0.0000	1.000
8	0.0001	0.0002	0.1037	0.216	0.354	0.1037	0.0513	0.8770	0.0000	1.000
9	0.0000	0.0002	0.8150	0.217	0.354	0.8150	0.0513	0.8770	0.0000	1.231
10	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
11	0.0001	0.0001	0.1045	0.216	0.354	0.1045	3.0513	0.8770	0.0000	1.000
12	0.0001	0.0001	0.5877	0.216	0.354	0.5877	0.0513	0.8770	0.0000	1.000
13	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
14	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
15	0.0001	0.0002	0.1558	0.216	0.354	0.1558	0.0513	0.8770	0.0000	1.000
16	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	3.0000	1.000
17	0.0001	0.0002	0.8147	0.216	0.354	0.8147	0.0513	0.8770	0.0000	1.001
18	0.0002	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	3.0000	1.000
19	0.0001	0.0002	0.8150	0.216	0.354	0.8150	3.0513	0.8770	0.0000	1.000
20	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
21	0.0002	0.0001	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
22	0.0002	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
23	0.0001	0.0002	0.1038	0.216	0.354	0.1038	3.0513	0.8770	0.0000	1.000
24	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
25	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.231
26	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	3.0000	1.000
27	0.0000	0.0002	0.8150	0.217	0.354	0.8150	3.0513	0.8770	0.0000	1.001
28	0.0001	0.0001	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
29	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
30	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
31	0.0002	0.0002	0.8150	0.216	0.354	0.8150	3.0513	0.8770	0.0000	1.000
32	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
33	0.0000	0.0002	0.8150	0.217	0.354	0.8150	3.0513	0.8770	0.0000	1.000
34	0.0002	0.0002	0.1608	0.216	0.354	0.1608	0.0513	0.8770	0.0000	1.000
35	0.0002	0.0002	0.8150	0.216	0.354	0.8150	3.0513	0.8770	0.0000	1.000
36	0.0001	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000
37	0.0001	0.0001	0.5810	0.216	0.354	0.5810	0.0513	0.8770	0.0000	1.000
38	0.0002	0.0002	0.8150	0.216	0.354	0.8150	0.0513	0.8770	0.0000	1.000

BASE BALANCE

TOTAL MASS OF OIL SPILLED 10000.00000 SPILL TIME

LOCATION OF OIL OR SPILLAGE	AMOUNT (SPILL TIME)	PERCENT OF TOTAL
	2333.33333	23.33
	7666.66667	76.67

TO OILSP COLLEGE OR SPILLER OR OILSP	TO OILSP PARTICLES OR DEPOSITED PARTICLES	AMOUNT	PERCENT
		10.00000	0.10
		20.33333	0.20
		0.00000	0.00
REMOVED PARTICLES		0.00000	0.00
PHYSICALLY CLARIFIED		0.00000	0.00
LOST FROM OILSP HOLDINGS	0 LOST PARTICLES	0.00000	0.00

SPILL CONTROL PARAMETERS... 1.0000... 0.0000... 0.0000... 0.0000... 0.0000... 0.0000... 0.0000... 0.0000...

PERFORMANCE DATA SPILL THIS OILSP: SPILL

CLARIFIED

AMOUNT OF SPILLERS OR SPILL CONTROL SPILLS THIS OILSP: 1 SPILLERS: 0 CLARIFIED SPILLS: 1 OILSPERS SPILLS:

Figure VIII.-7. Output from Main Simulation

WIND VELOCITY INPUT DATA 1.00 HOURS AFTER THE OCCURRENCE OF THE SPELL

THE WIND VELOCITY GRID HAS 1 DIVISIONS IN X SPACE 0.5000 DEGREES APART
 AND 1 DIVISIONS IN Y SPACE 0.2500 DEGREES APART.

THE (1,1) GRID LOCATION OF THE WIND VELOCITY COORDINATE SYSTEM IS AT 48.00000 DEGREES LONGITUDE AND 61.25000 DEGREES LATITUDE

N VALUES IN UNITS OF M/S

Y PLPAPPTS 1
 1 0.000

E PLPAPPTS 1
 1 -4.190

WIND CURRENT VELOCITY DATA 1.00 HOURS AFTER THE OCCURRENCE OF THE SPELL

THE WIND CURRENT VELOCITY GRID HAS 10 DIVISIONS IN X SPACE 0.0500 DEGREES APART
 AND 10 DIVISIONS IN Y SPACE 0.0500 DEGREES APART.

THE (1,1) GRID LOCATION OF THE WIND CURRENT VELOCITY COORDINATE SYSTEM IS AT 47.00000 DEGREES LONGITUDE AND 61.25000 DEGREES LATITUDE

ALL VALUES AND POSITIONS HAVE BEEN DIVIDED BY 10 TO -4

N VALUES IN UNITS OF M/S

Y PLPAPPTS	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	0.600	0.600	0.600	0.611	0.665	0.710	0.676	0.657	0.661	0.699	1.026	1.260	0.122	1.215
11	0.606	0.606	0.606	0.678	0.611	0.638	0.625	1.084	0.671	0.676	0.617	0.616	0.609	0.287
12	0.600	0.600	0.600	0.683	0.695	0.675	0.658	0.600	0.640	0.618	0.701	0.640	0.699	0.686
11	0.601	0.601	0.627	0.111	0.161	0.612	0.791	0.610	0.665	0.797	0.720	0.670	0.661	0.670
10	0.600	0.600	0.600	0.600	0.665	0.100	0.710	0.764	0.621	0.770	1.705	1.760	0.681	0.676
9	0.607	0.607	0.607	0.607	0.607	0.205	0.711	0.710	0.690	1.681	0.607	0.611	0.771	0.661
8	0.600	0.600	0.600	0.600	0.670	0.205	0.680	0.686	0.605	1.660	0.707	0.772	0.690	1.516
7	0.252	0.780	0.100	0.082	0.161	0.717	0.671	0.610	0.601	0.597	0.665	1.589	0.670	0.612
6	0.282	0.600	0.101	0.102	0.212	0.120	0.100	0.347	0.600	0.327	0.647	0.602	0.600	0.620
5	0.231	0.229	0.182	0.167	0.081	-0.176	0.633	-0.010	-0.170	-0.125	0.202	0.176	0.600	0.670
4	0.250	0.255	0.125	0.209	0.111	-0.011	0.150	0.071	-0.116	1.009	0.106	0.297	0.107	0.152
3	0.270	0.267	0.260	0.255	0.100	0.111	0.266	0.176	0.067	0.277	0.161	1.210	0.196	0.227
2	0.290	0.279	0.256	0.251	0.210	0.195	0.260	0.107	0.102	1.107	0.100	1.210	0.212	0.201
1	0.103	0.275	0.281	0.280	0.270	0.277	0.262	0.210	0.107	1.111	0.107	0.212	0.212	0.251

Figure VIII.-7. Output from Main Simulation

OIL SPILL DISPERSION MODEL - 3.00 HOURS AFTER THE OCCURRENCE OF THE SPILL

THE OIL SPILL OCCURRED AT 00:00 HOURS AT LOCATION 44, 8121000 AND LATITUDE 01, 400000
 IN A DIRECTION TO Y EAST AND IN A DIRECTION TO X SOUTH

THE (1,1) OIL LOCATION OF THE OIL SPILL CENTER POINT SYSTEM IS AT 47,000000 LONGITUDE AND 01,300000 LATITUDE

ALL VALUES AND PROBABILITIES WERE DIVIDED BY 10 TO -4

VALUES IN UNITS OF M/S

Y PLUMBOUS	Y PLUMBOUS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	0.205	0.205	0.205	-0.124	-0.117	-0.030	0.127	0.175	0.501	0.612	1.729	1.901	0.740	0.490
11	0.205	0.205	0.205	-0.009	-0.209	0.052	0.107	0.000	0.527	0.612	0.507	0.075	0.700	0.710
12	0.205	0.205	0.205	-0.154	-0.105	0.001	0.100	0.118	0.011	0.055	0.005	1.711	0.001	0.670
13	0.205	0.205	-0.124	-0.101	-0.101	0.111	0.142	0.251	0.165	1.005	0.075	0.600	0.705	0.400
10	0.205	0.205	0.205	0.205	-0.150	0.010	0.155	0.201	0.205	1.210	0.210	0.200	0.210	0.201
0	0.205	0.205	0.205	0.205	-0.157	-0.101	0.107	0.142	0.050	0.057	-0.011	-0.011	-0.107	-0.100
0	0.205	0.205	0.205	0.205	-0.100	-0.017	0.102	1.120	0.075	0.015	-0.075	0.007	-0.110	-0.112
7	-0.170	0.617	0.720	0.250	-0.070	-0.010	0.070	0.001	0.007	1.071	-0.050	-0.110	-0.007	-0.071
6	0.054	0.110	0.577	0.200	0.201	0.116	-0.010	-0.010	0.110	1.175	-0.007	-0.000	-0.071	-0.075
5	0.207	0.041	0.026	0.210	0.005	0.001	-0.201	-0.211	0.110	0.007	-0.110	-0.007	-0.000	-0.017
0	0.110	0.005	0.100	0.007	0.250	0.100	-0.210	-0.150	0.100	0.101	-1.151	1.331	0.050	0.040
1	-0.007	-0.051	-0.000	-0.000	-0.152	-0.111	-0.210	-0.110	-0.271	-1.077	0.011	0.101	0.107	0.107
2	-0.021	-0.016	0.000	0.005	-0.101	-0.007	-0.112	-0.000	-0.051	1.010	1.070	1.301	0.110	0.107
1	0.000	0.010	0.057	0.055	-0.055	-0.001	-0.055	-0.077	0.011	0.057	0.300	1.101	0.001	0.100

EXISTING SPILLS - 1,000 MILES AFTER THE OCCURRENCE OF THE SPILL

SPILLS OCCURRED DURING THIS YEAR

THE 1 SPILL OCCURRED 0.00 HOURS AFTER THE OCCURRENCE OF THE SPILL
 IT IS CENTERED AT LONGITUDE 44,812100 AND LATITUDE 01,400000
 IN A DIRECTION TO Y EAST AND IN A DIRECTION TO X SOUTH

COMP PROPERTIES OF THE SPILLED OIL ARE:

PROBABILITY	1.000000	PROPERTIES	0.000000
INTERFACIAL TENSION	10.000000	PROPERTIES	0.000000
DIFFUSION COEFFICIENT	1.000000	PROPERTIES	0.000000

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C ₁₀ -C ₁₂)	0.004000
PARAFFIN (C ₁₃ -C ₂₂)	1.000000
AROMATIC (C ₁₀ -C ₁₂)	0.000000
AROMATIC (C ₁₃ -C ₂₂)	0.000000
AROMATIC (C ₂₃ -C ₃₀)	0.000000
AROMATIC (C ₃₁ -C ₄₀)	0.000000
AROMATIC (C ₄₁ -C ₅₀)	0.000000
AROMATIC (C ₅₁ -C ₆₀)	0.000000

THE 2 SPILLS OCCURRED DURING THIS YEAR

THE 2 SPILLS OCCURRED 1.00 HOURS AFTER THE OCCURRENCE OF THE SPILL
 IT IS CENTERED AT LONGITUDE 44,820000 AND LATITUDE 01,400000
 IN A DIRECTION TO Y EAST AND IN A DIRECTION TO X SOUTH

COMP PROPERTIES OF THE SPILLED OIL ARE:

PROBABILITY	0.000000	PROPERTIES	0.000000
INTERFACIAL TENSION	10.000000	PROPERTIES	0.000000
DIFFUSION COEFFICIENT	1.000000	PROPERTIES	0.000000

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C ₁₀ -C ₁₂)	1.000000
PARAFFIN (C ₁₃ -C ₂₂)	0.000000
AROMATIC (C ₁₀ -C ₁₂)	0.000000
AROMATIC (C ₁₃ -C ₂₂)	0.000000
AROMATIC (C ₂₃ -C ₃₀)	0.000000
AROMATIC (C ₃₁ -C ₄₀)	0.000000
AROMATIC (C ₄₁ -C ₅₀)	0.000000
AROMATIC (C ₅₁ -C ₆₀)	0.000000

EXISTING OIL DISPERSION AND DAMAGE LOCATION STATISTICS

NUMBER OF BEACHING GRID IS AT 1 0.0000 0.0000 IN A DIRECTION TO Y EAST AND IN A DIRECTION TO X SOUTH
 THE BEACH GRID COORDINATE IN THE BEACHING SYSTEM IS 0.000000 LONGITUDE IN Y AND 1.000000 LATITUDE IN X
 THE GRID COORDINATE IN THE BEACH SYSTEM IS 0.000000 LONGITUDE IN Y AND 0.000000 LATITUDE IN X

THE BEACHING BEACH IS AT 1 0.000000 0.000000
 THE BEACHING BEACHING IS AT 0.000000 0.000000
 THE BEACHING BEACHING IS AT 0.000000 0.000000
 THE BEACHING BEACHING IS AT 0.000000 0.000000

Figure VIII.-7. Output from Main Simulation

ALL HORIZONTAL VELOCITIES ARE MULTIPLIED BY 10000

U VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	0.312	0.166	0.000	0.052	0.010		
0.2	0.211	0.278	0.271	0.118	0.152		
0.2	0.010	0.026	0.037	0.000	0.511		
0.2	0.001	0.057	0.000	0.001	0.710		
0.1	0.070	0.718	0.702	0.765	0.767		

U VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 2	
0.2	0.312	0.166	0.000	0.052	0.010		
0.2	0.211	0.278	0.271	0.118	0.152		
0.2	0.010	0.026	0.037	0.000	0.511		
0.2	0.001	0.057	0.000	0.001	0.710		
0.1	0.070	0.718	0.702	0.765	0.767		

U VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	0.312	0.166	0.000	0.052	0.010		
0.2	0.211	0.278	0.271	0.118	0.152		
0.2	0.010	0.026	0.037	0.000	0.511		
0.2	0.001	0.057	0.000	0.001	0.710		
0.1	0.070	0.718	0.702	0.765	0.767		

V VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	-0.152	-0.007	-0.018	-0.000	-0.000		
0.2	-0.118	-0.071	-0.023	-0.010	0.000		
0.2	-0.021	-0.051	-0.000	0.000	0.007		
0.2	0.077	0.000	0.007	0.100	0.111		
0.1	0.207	0.162	0.170	0.160	0.100		

V VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 2	
0.2	-0.152	-0.007	-0.018	-0.000	-0.000		
0.2	-0.118	-0.071	-0.023	-0.010	0.000		
0.2	-0.021	-0.051	-0.000	0.000	0.007		
0.2	0.077	0.000	0.007	0.100	0.111		
0.1	0.207	0.162	0.170	0.160	0.100		

V VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	-0.152	-0.007	-0.018	-0.000	-0.000		
0.2	-0.118	-0.071	-0.023	-0.010	0.000		
0.2	-0.021	-0.051	-0.000	0.000	0.007		
0.2	0.077	0.000	0.007	0.100	0.111		
0.1	0.207	0.162	0.170	0.160	0.100		

W VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.1	0.000	0.000	0.000	0.000	0.000		

W VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 2	
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.1	0.000	0.000	0.000	0.000	0.000		

W VELOCITY FIELD		STEP NUMBER		TIME		LEVEL	
0.1	0.33	0.18	0.16	0.37	10000.00	LEVEL 1	
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.2	0.000	0.000	0.000	0.000	0.000		
0.1	0.000	0.000	0.000	0.000	0.000		

FLOATING GRID POSITION AND PARTICLE LOCATION STATISTICS

THE CENTER OF FLOATING GRID IS AT (0.1027, 0.1010) IN COORDINATES WITH RESPECT TO THE ORIGIN OF THE FIELD APPROX ORIGIN
 THE RMS GRID SEPARATION IN THE FLOATING SYSTEM IS 0.070000 IN X AND 0.060000 IN Y
 THE GRID SEPARATION IN THE FIELD SYSTEM IS 0.010000 IN X AND 0.010000 IN Y

THE APPROX VALUES OF X, Y AND Z ARE 0.017000 0.000000 0.160000
 THE STANDARD DEVIATIONS ARE 0.001000 0.000000 0.121000

Figure VIII.-7. Output from Main Simulation

```

CONCENTRATION IN % OF OIL PER ML OF WATER      STEP NUMBER 1      TIME 1000.00 LEVEL 1
0.11 0.11 0.10 0.10 0.17
0.19 0.0000 0.0000 0.0000 0.0000 0.0000
0.21 0.0000 0.0000 0.0000 0.0000 0.0000
0.22 0.0000 0.0000 0.0000 0.0000 0.0000
0.24 0.0000 0.0000 0.0000 0.0000 0.0000
0.25 0.0000 0.0000 0.0000 0.0000 0.0000

CONCENTRATION IN % OF OIL PER ML OF WATER      STEP NUMBER 1      TIME 1000.00 LEVEL 2
0.11 0.11 0.10 0.10 0.17
0.19 0.0000 0.0000 0.0000 0.0000 0.0000
0.21 0.0000 0.0000 0.0000 0.0000 0.0000
0.22 0.0000 0.0000 0.0000 0.0000 0.0000
0.24 0.0000 0.0000 0.0000 0.0000 0.0000
0.25 0.0000 0.0000 0.0000 0.0000 0.0000

CONCENTRATION IN % OF OIL PER ML OF WATER      STEP NUMBER 1      TIME 1000.00 LEVEL 3
0.11 0.11 0.10 0.10 0.17
0.19 0.0000 0.0000 0.0000 0.0000 0.0000
0.21 0.0000 0.0000 0.0000 0.0000 0.0000
0.22 0.0000 0.0000 0.0000 0.0000 0.0000
0.24 0.0000 0.0000 0.0000 0.0000 0.0000
0.25 0.0000 0.0000 0.0000 0.0000 0.0000

```

SPILL CONTROL PARAMETERS.....0.000.00000 BEFORE THE BEGINNING OF THE SPILL.

```

ENVIRONMENTAL DATA FROM THIS STEP:          STEP
EMULSION OF SPILLERS OR SPILL CONTROL REPORTS THIS STEP: 0 SPILLERS; 0 CLEANUP REPORTS; 0 TREATMENT REPORTS.

```

EXISTING SPILLERS.....0.000.00000 BEFORE THE BEGINNING OF THE SPILL

SPILLERS CREATED PRIOR TO THIS STEP

```

STEP 1 SPILLER APPROX 0.00.0000 BEFORE THE BEGINNING OF THE SPILL
IT IS CREATED AT LONGITUDE 46.740710 AND LATITUDE 41.421140,
IS OF RADIO 1000.00 METERS AND IS OF WEIGHT 7100.0000 METRIC TONS.
SOME PROPERTIES OF THE SPILLER OIL ARE:
    DENSITY 1.010000 G/CM3
    INTERFACIAL TENSION 10.000000 DYNES/CM
    KINEMATIC VISCOSITY 1.000000 CM2/SEC
BY WEIGHT THE OIL FRACTIONS ARE:
    PARAFFIN (C14-C17) 0.000100
    PARAFFIN (C18-C21) 0.000000
    CYCLOPARAFFIN (C14-C17) 0.000000
    CYCLOPARAFFIN (C18-C21) 0.000000
    AROMATIC (C6-C11) 0.000000
    AROMATIC (C12-C14) 0.000000
    AROMATIC-CONDENSATED (C6-C14) 0.000000
    RESIDUAL 0.000000

STEP 2 SPILLER APPROX 1.00.0000 BEFORE THE BEGINNING OF THE SPILL
IT IS CREATED AT LONGITUDE 46.802710 AND LATITUDE 41.400110,
IS OF RADIO 1000.00 METERS AND IS OF WEIGHT 7100.0000 METRIC TONS.
SOME PROPERTIES OF THE SPILLER OIL ARE:
    DENSITY 1.000000 G/CM3
    INTERFACIAL TENSION 10.000000 DYNES/CM
    KINEMATIC VISCOSITY 1.000000 CM2/SEC
BY WEIGHT THE OIL FRACTIONS ARE:
    PARAFFIN (C14-C17) 0.000100
    PARAFFIN (C18-C21) 0.000000
    CYCLOPARAFFIN (C14-C17) 0.000000
    CYCLOPARAFFIN (C18-C21) 0.000000
    AROMATIC (C6-C11) 0.000000
    AROMATIC (C12-C14) 0.000000
    AROMATIC-CONDENSATED (C6-C14) 0.000000
    RESIDUAL 0.000000

```

FLOATING GRID DEPOSITION AND PARTICLE LOCATION STATISTICS

```

THE SIZE OF FLOATING GRID IS AT X 0.1700, Y 0.2420, Z 0.000000 WITH RESPECT TO THE CENTER OF THE SPILLER OIL
THE SPILLER OIL DEPOSITION IN THE FLOATING GRID IS 0.000000 G/CM2 WITH RESPECT TO THE CENTER OF THE SPILLER OIL
THE GRID DEPOSITION IN THE SPILLER OIL IS 0.000000 G/CM2 WITH RESPECT TO THE CENTER OF THE SPILLER OIL
THE AVERAGE VALUES OF X, Y AND Z ARE 0.170000, 0.242000, 0.000000
THE STANDARD DEVIATIONS ARE 0.000000, 0.000000, 0.000000

```

Figure VIII.-7. Output from Main Simulation

***** PARTICLE POSITIONS AT END OF THE PLASMA SYSTEM IN SIMULATION *****
 PARTICLE SEPARATIONS BY TIME 10000.00

ID	PARTICLE POSITION PLASMA SYSTEM			PARTICLE POSITION FIELD SYSTEM			SEPARATION	DENSITY	SP. CHG.	MOM
	X	Y	Z	X	Y	Z				
1	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
2	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
3	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
4	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
5	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
6	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
7	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
8	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
9	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
10	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
11	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
12	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
13	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
14	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
15	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
16	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
17	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
18	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
19	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
20	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
21	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
22	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
23	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
24	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
25	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
26	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
27	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
28	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
29	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
30	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
31	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
32	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
33	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
34	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
35	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
36	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
37	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
38	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
39	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
40	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
41	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
42	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
43	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
44	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
45	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
46	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
47	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
48	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
49	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000
50	0.0170	0.0514	0.0140	0.220	0.155	0.0140	0.0013	0.0770	0.0000	0.000

Figure VIII.-7. Output from Main Simulation

WYD CHOPPY TEND DATA K.00 WYD WYD WYD WYD WYD

THE WYD CHOPPY GRID HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPARE
AND 10 DIVISIONS IN Y SPACE 0.1157 DEGREES SPARE.

THE (1,1) GRID LOCATION OF THE WYD CHOPPY COMPUTATION SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT WYD WYD DISTOP BY 10 ** -4

WYD CHOPPY TEND DATA K.00 WYD WYD WYD WYD WYD

THE WYD CHOPPY GRID HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPARE
AND 10 DIVISIONS IN Y SPACE 0.1157 DEGREES SPARE.

THE (1,1) GRID LOCATION OF THE WYD CHOPPY COMPUTATION SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT WYD WYD DISTOP BY 10 ** -4

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	0.130	0.130	0.130	-0.037	-0.005	0.285	0.507	0.897	0.512	1.828	0.855	0.277	-0.188	-0.235
11	0.130	0.130	0.130	0.107	0.183	0.870	0.857	0.578	0.501	0.872	0.388	0.160	-0.058	-0.181
12	0.130	0.130	0.130	-0.028	0.028	0.208	0.102	0.828	0.888	0.388	0.277	0.218	0.011	0.181
11	0.137	0.137	0.163	-0.153	-0.083	-0.057	0.177	0.350	0.501	0.371	1.255	1.118	0.078	0.160
10	0.137	0.137	0.137	0.137	-0.017	-0.158	0.277	0.388	0.858	0.258	0.318	0.388	0.188	0.218
9	0.136	0.136	0.136	0.136	0.087	-0.258	0.251	0.250	0.878	0.210	0.827	0.881	0.317	0.180
8	0.136	0.136	0.136	0.136	-0.035	-0.258	0.180	0.277	0.187	0.205	0.118	1.118	0.288	0.077
7	-0.205	0.281	-0.151	-0.815	-0.118	-0.220	0.118	0.157	0.188	0.180	0.188	0.188	0.212	0.121
6	-0.213	0.028	-0.112	-0.183	-0.283	-0.111	-0.035	-0.088	-0.088	-0.128	0.812	0.117	0.058	0.058
5	-0.222	-0.228	-0.071	-0.281	-0.110	-0.628	-0.828	-0.888	-0.878	-0.878	-0.878	-0.878	-0.878	-0.878
4	-0.188	-0.188	-0.127	-0.282	-0.181	-0.883	-0.102	-0.181	-0.588	-0.801	-0.255	-0.160	-0.158	-0.088
3	-0.172	-0.168	-0.181	-0.188	-0.110	-0.110	-0.188	-0.275	-0.151	-0.210	-0.258	-0.288	-0.258	-0.221
2	-0.158	-0.168	-0.181	-0.187	-0.218	-0.258	-0.188	-0.251	-0.188	-0.251	-0.251	-0.218	-0.218	-0.288
1	-0.188	-0.171	-0.208	-0.188	-0.168	-0.178	-0.185	-0.228	-0.268	-0.278	-0.258	-0.235	-0.218	-0.188

WYD CHOPPY TEND DATA K.00 WYD WYD WYD WYD WYD

THE WYD CHOPPY GRID HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPARE
AND 10 DIVISIONS IN Y SPACE 0.1157 DEGREES SPARE.

THE (1,1) GRID LOCATION OF THE WYD CHOPPY COMPUTATION SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT WYD WYD DISTOP BY 10 ** -4

WYD CHOPPY TEND DATA K.00 WYD WYD WYD WYD WYD

THE WYD CHOPPY GRID HAS 10 DIVISIONS IN X SPACE 0.0157 DEGREES SPARE
AND 10 DIVISIONS IN Y SPACE 0.1157 DEGREES SPARE.

THE (1,1) GRID LOCATION OF THE WYD CHOPPY COMPUTATION SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 61.10000 DEGREES LATITUDE

ALL VALUES FOR PRINTOUT WYD WYD DISTOP BY 10 ** -4

Y ELEMENTS	X ELEMENTS													
	1	2	3	4	5	6	7	8	9	10	11	12	13	14
10	-0.181	-0.181	-0.181	-0.152	-0.162	-0.855	-0.181	-0.058	0.115	0.188	1.202	0.878	0.111	0.168
11	-0.181	-0.181	-0.181	-0.818	-0.818	-0.371	-0.278	0.018	0.055	0.147	0.181	0.850	0.371	0.118
12	-0.181	-0.181	-0.181	-0.782	-0.621	-0.111	-0.288	-0.112	-0.018	1.011	0.071	0.288	0.218	0.251
11	-0.181	-0.181	-0.752	-0.728	-0.688	-0.282	-0.288	-0.178	-0.068	-0.021	1.888	1.181	0.118	0.222
10	-0.181	-0.181	-0.181	-0.181	-0.585	-0.811	-0.271	-0.225	-0.218	-0.211	-0.211	-0.127	-0.288	-0.188
9	-0.181	-0.181	-0.181	-0.181	-0.582	-0.528	-0.278	-0.288	-0.271	-0.275	-0.858	-0.857	-0.571	-0.511
8	-0.181	-0.181	-0.181	-0.181	-0.511	-0.858	-0.288	-0.287	-0.187	-0.188	-0.851	-0.818	-0.581	-0.517
7	-0.585	0.182	0.301	-0.187	-0.588	-0.888	-0.350	-0.188	-0.818	-0.158	-0.888	-0.581	-0.881	-0.888
6	-0.170	-0.088	0.152	-0.177	-0.112	-0.280	-0.861	-0.855	-0.311	-0.250	-0.511	-0.528	-0.888	-0.500
5	-0.181	-0.188	0.081	-0.187	0.218	0.088	-0.688	-0.618	-0.085	-0.871	-0.581	-0.888	-0.871	-0.882
4	-0.188	-0.828	-0.217	-0.128	-0.168	-0.288	-0.661	-0.582	-0.121	-0.215	-0.877	-0.385	-0.375	-0.385
3	-0.872	-0.877	-0.875	-0.888	-0.577	-0.557	-0.615	-0.525	-0.585	-0.117	-0.812	-0.322	-0.278	-0.218
2	-0.888	-0.882	-0.827	-0.828	-0.528	-0.521	-0.558	-0.888	-0.878	-0.588	-0.187	-0.181	-0.118	-0.278
1	-0.825	-0.888	-0.168	-0.171	-0.888	-0.888	-0.888	-0.887	-0.811	-0.371	-0.381	-0.168	-0.381	-0.317

Figure VIII.-7. Output from Main Simulation

PLASTIC SPILLAGE.....6,000,000000 AFTER THE RECEIVING OF THE OIL

SPILLAGE CAPTURED PRIOR TO THIS STEP

STEP 1 SPILLAGE APPARUS 0.00 HOURS AFTER THE RECEIVING OF THE OIL
IT IS CONTROLLED BY LONGITUDE 44.818400 AND LATITUDE 81.451200,
IS OF RADIUS 1000.71 APPROX AND IS OF WEIGHT 7000.6400 APPROX TONS.
SUMP PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 1.000000 G/CM3
INTERFACIAL TENSION 10.000000 DYNES/CM
DIPNETIC VISCOSITY 1.000000 CENTISTOINES
BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C4-C12) 3.002222
PARAFFIN (C13-C22) 0.000000
CYCLOPARAFFIN (C4-C12) 0.000000
CYCLOPARAFFIN (C13-C22) 0.000000
AROMATIC (C4-C12) 0.000000
AROMATIC (C13-C18) 0.000000
SATURATED-AROMATIC (C9-C24) 0.000000
RESIDUAL 0.000000

STEP 2 SPILLAGE APPARUS 1.00 HOURS AFTER THE RECEIVING OF THE OIL
IT IS CONTROLLED BY LONGITUDE 44.818400 AND LATITUDE 81.451200,
IS OF RADIUS 1000.71 APPROX AND IS OF WEIGHT 7000.6400 APPROX TONS.
SUMP PROPERTIES OF THE SPILLED OIL ARE:

DENSITY 0.985200 G/CM3
INTERFACIAL TENSION 10.000000 DYNES/CM
DIPNETIC VISCOSITY 1.000000 CENTISTOINES
BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C4-C12) 3.010000
PARAFFIN (C13-C22) 0.000000
CYCLOPARAFFIN (C4-C12) 0.000000
CYCLOPARAFFIN (C13-C22) 0.000000
AROMATIC (C4-C12) 0.000000
AROMATIC (C13-C18) 0.000000
SATURATED-AROMATIC (C9-C24) 0.000000
RESIDUAL 0.000000

MOVING GRID ORIGIN AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT X 0.1927, 0.2728 IN APPROX WITH RESPECT TO THE ORIGIN OF THE FIXED REFER GRID
THE GRID SEPARATION IN THE FLOATING X-SECTION IS 0.017000 APPROX IN Z AND 0.017000 APPROX IN Y
THE GRID SEPARATION IN THE FIXED X-SECTION IS 0.016 APPROX IN Z AND 0.016 APPROX IN Y

THE APPROX VALUES OF X, Y AND Z ARE 0.018157 0.078210 0.272820
THE STANDARD DEVIATIONS ARE 0.006114 0.012152 0.551003
HORIZONTAL E-Z CORRELATION COEFFICIENT 0.28107-04 0.13010-14
E-W CORRELATION COEFFICIENT 0.1017-01 0.1017-01 0.1017-01

	0.28	0.11	0.11	0.16	0.18
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000	0.000

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH
0.28	0.11	0.11	0.16	0.18
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000

MOVING GRID ORIGIN AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT X 0.1700, 0.2676 IN APPROX WITH RESPECT TO THE ORIGIN OF THE FIXED REFER GRID
THE GRID SEPARATION IN THE FLOATING X-SECTION IS 0.010200 APPROX IN Z AND 0.010200 APPROX IN Y
THE GRID SEPARATION IN THE FIXED X-SECTION IS 0.016 APPROX IN Z AND 0.016 APPROX IN Y

THE APPROX VALUES OF X, Y AND Z ARE 0.000007 0.078140 0.266100
THE STANDARD DEVIATIONS ARE 0.000571 0.012070 0.130512

81. HORIZONTAL VELOCITY AND VELOCITY AT 10000

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH	
0.28	0.11	0.11	0.16	0.18	
0.2	-0.251	-0.168	-0.106	-0.038	-0.036
0.2	-0.116	-0.176	-0.201	-0.181	-0.081
0.2	0.087	0.081	0.086	0.048	0.127
0.2	0.188	0.206	0.267	0.101	0.108
0.1	0.205	0.225	0.264	0.107	0.121

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH	
0.28	0.11	0.11	0.16	0.18	
0.2	-0.251	-0.168	-0.106	-0.038	-0.036
0.2	-0.116	-0.176	-0.201	-0.181	-0.081
0.2	0.087	0.081	0.086	0.048	0.127
0.2	0.188	0.206	0.267	0.101	0.108
0.1	0.205	0.225	0.264	0.107	0.121

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH	
0.28	0.11	0.11	0.16	0.18	
0.2	-0.527	-0.576	-0.676	-0.887	-0.808
0.2	-0.480	-0.538	-0.640	-0.807	-0.121
0.2	-0.184	-0.818	-0.888	-0.167	-0.157
0.2	-0.282	-0.118	-0.118	-0.281	-0.288
0.1	-0.250	-0.228	-0.288	-0.281	-0.288

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH	
0.28	0.11	0.11	0.16	0.18	
0.2	-0.527	-0.576	-0.676	-0.887	-0.808
0.2	-0.480	-0.538	-0.640	-0.807	-0.121
0.2	-0.184	-0.818	-0.888	-0.167	-0.157
0.2	-0.282	-0.118	-0.118	-0.281	-0.288
0.1	-0.250	-0.228	-0.288	-0.281	-0.288

U VELOCITY FIELD	STP NUMBER	Z	TIME	DEPTH	
0.28	0.11	0.11	0.16	0.18	
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000	0.000

Figure VIII.-7. Output from Main Simulation

CONCENTRATION IN MG OF OIL PER ML OF WATER						STPP NUMBER	2	TEMP	21657.30	LEVEL	1
0.14	0.24	0.11	0.17	0.16	0.18						
0.21	0.0000	0.0000	0.0000	0.0000	0.0000						
0.21	0.0000	0.0000	0.0015	0.0008	0.0000						
0.21	0.0000	0.0000	0.0017	0.0015	0.0000						
0.24	0.0000	0.0000	0.0000	0.0000	0.0000						
0.24	0.0000	0.0000	0.0000	0.0000	0.0000						

CONCENTRATION IN MG OF OIL PER ML OF WATER						STPP NUMBER	2	TEMP	21500.30	LEVEL	2
0.14	0.24	0.11	0.17	0.16	0.18						
0.21	0.0000	0.0000	0.0000	0.0000	0.0000						
0.21	0.0000	0.0000	0.0028	0.0020	0.0000						
0.21	0.0000	0.0014	0.0057	0.0037	0.0000						
0.24	0.0000	0.0000	0.0000	0.0000	0.0000						
0.24	0.0000	0.0000	0.0000	0.0000	0.0000						

CONCENTRATION IN MG OF OIL PER ML OF WATER						STPP NUMBER	2	TEMP	21607.30	LEVEL	1
0.14	0.24	0.11	0.17	0.16	0.18						
0.21	0.0000	0.0000	0.0000	0.0000	0.0000						
0.21	0.0000	0.0018	0.0082	0.0221	0.0000						
0.24	0.0000	0.0000	0.0015	0.0014	0.0000						
0.24	0.0000	0.0000	0.0000	0.0000	0.0000						

PARTICLE POSITIONS IN AND WITH THE FLOATING SYSTEM IN DEGREES 2 IN STPP NO. 2
PARTICLE PARAMETERS BY TIME 21600.30

P	PARTICLE POSITION IN FLOATING SYSTEM			PARTICLE POSITION IN STPP			DEGREE	TEMP	LEVEL	WAVE
	X	Y	Z	X	Y	Z				
1	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
2	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
3	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
4	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
5	0.0000	0.0026	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
6	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
7	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
8	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
9	0.0002	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
10	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
11	0.0001	0.0026	0.8145	0.210	0.150	0.8145	0.0013	0.8770	0.0000	0.000
12	0.0001	0.0026	0.8172	0.210	0.150	0.8172	0.0013	0.8770	0.0000	0.000
13	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
14	0.0000	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
15	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
16	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
17	0.0000	0.0027	0.8167	0.210	0.150	0.8167	0.0013	0.8770	0.0000	0.000
18	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
19	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
20	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
21	0.0000	0.0028	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
22	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
23	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
24	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
25	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
26	0.0002	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
27	0.0001	0.0028	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
28	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
29	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
30	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
31	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
32	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
33	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
34	0.0000	0.0026	0.8100	0.210	0.150	0.8100	0.0010	0.8770	0.0000	0.000
35	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
36	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
37	0.0001	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
38	0.0000	0.0027	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
39	0.0000	0.0026	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
40	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0010	0.8770	0.0000	0.000
41	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
42	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
43	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
44	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
45	0.0002	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
46	0.0004	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
47	0.0001	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
48	0.0001	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
49	0.0001	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000
50	0.0001	0.0026	0.8150	0.210	0.150	0.8150	0.0013	0.8770	0.0000	0.000

Figure VIII.-7. Output from Main

51	0.0010	0.0700	0.0150	0.270	0.102	0.0150	0.0010	1.0512	0.0000	1.001
52	0.0020	0.0420	0.0150	0.221	0.110	0.0150	0.0010	1.0012	0.0000	1.001
53	0.0001	0.0670	0.0150	0.221	0.100	0.0150	0.0010	1.0112	0.0000	1.001
54	0.0070	0.0675	0.0150	0.221	0.100	0.0150	0.0010	1.0012	0.0000	1.001
55	0.0172	0.0015	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
56	0.0152	0.0150	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
57	0.0002	0.0000	0.0150	0.210	0.102	0.0150	0.0010	1.0012	0.0000	1.001
58	0.0111	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
59	0.0000	0.0000	0.0150	0.210	0.100	0.0150	0.0010	1.0012	0.0000	1.001
60	0.0011	0.0020	0.0150	0.222	0.110	0.0150	0.0010	1.0012	0.0000	1.001
61	0.0200	0.0020	0.0150	0.211	0.110	0.0150	0.0010	1.0012	0.0000	1.001
62	0.0101	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
63	0.0012	0.0000	0.0150	0.220	0.120	0.0150	0.0010	1.0012	0.0000	1.001
64	0.0010	0.0010	0.0150	0.210	0.120	0.0150	0.0010	1.0012	0.0000	1.001
65	0.0020	0.0010	0.0150	0.221	0.120	0.0150	0.0010	1.0012	0.0000	1.001
66	0.0001	0.0000	0.0150	0.221	0.120	0.0150	0.0010	1.0012	0.0000	1.001
67	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
68	0.0010	0.0010	0.0150	0.220	0.120	0.0150	0.0010	1.0012	0.0000	1.001
69	0.0010	0.0000	0.0150	0.222	0.110	0.0150	0.0010	1.0012	0.0000	1.001
70	0.0010	0.0010	0.0150	0.220	0.120	0.0150	0.0010	1.0012	0.0000	1.001
71	0.0001	0.0010	0.0150	0.221	0.111	0.0150	0.0010	1.0012	0.0000	1.001
72	0.0001	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
73	0.0100	0.0010	0.0150	0.212	0.151	0.0150	0.0010	1.0012	0.0000	0.000
74	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
75	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
76	0.0010	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
77	0.0101	0.0010	0.0150	0.212	0.151	0.0150	0.0010	1.0012	0.0000	0.000
78	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
79	0.0101	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
80	0.0100	0.0010	0.0150	0.212	0.151	0.0150	0.0010	1.0012	0.0000	0.000
81	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
82	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
83	0.0102	0.0010	0.0150	0.210	0.151	0.0150	0.0010	1.0012	0.0000	0.000
84	0.0010	0.0010	0.0150	0.220	0.111	0.0150	0.0010	1.0012	0.0000	0.000
85	0.0021	0.0150	0.0150	0.221	0.111	0.0150	0.0010	1.0012	0.0000	1.000
86	0.0012	0.0010	0.0150	0.220	0.110	0.0150	0.0010	1.0012	0.0000	1.000
87	0.0001	0.0010	0.0150	0.222	0.110	0.0150	0.0010	1.0012	0.0000	1.000
88	0.0010	0.0010	0.0150	0.220	0.110	0.0150	0.0010	1.0012	0.0000	1.000
89	0.0010	0.0010	0.0150	0.220	0.110	0.0150	0.0010	1.0012	0.0000	1.000
90	0.0010	0.0010	0.0150	0.220	0.110	0.0150	0.0010	1.0012	0.0000	1.000
91	0.0010	0.0010	0.0150	0.210	0.110	0.0150	0.0010	1.0012	0.0000	0.000
92	0.0021	0.0010	0.0150	0.221	0.110	0.0150	0.0010	1.0012	0.0000	0.000
93	0.0000	0.0010	0.0150	0.221	0.110	0.0150	0.0010	1.0012	0.0000	0.000
94	0.0010	0.0010	0.0150	0.210	0.110	0.0150	0.0010	1.0012	0.0000	0.000

SPSC RECEIPTS

TOTAL PAID BY ALL CITIES		19800,0000		00001 PAID	
INCREASE IN NET		AMOUNT (00001) PAID		PERCENT OF TOTAL	
TO STATEMENT		0010,0000		51.00	
TO COUNTY		1510,0000		7.50	
TO OTHER CITIES	40,000000	10,0000		0.07	
TO BONDS	47,000000	00,0000		0.00	
TO OTHER				0.00	
PERCENT CONTRIBUTION					
SPRINGFIELD COUNTY		0.0010		0.00	
SPRINGFIELD CITIES OF		0.0000		0.00	
LAST YEAR STATE BONDS	0.000000	0.0000		0.00	

Figure VIII.-7. Output from Main

ALL INDIVIDUAL VELOCITIES ARE MULTIPLIED BY 10000

U VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	1
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

V VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	2
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

W VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	3
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

X VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	4
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

Y VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	5
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

Z VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	6
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	-0.186	-0.152	-0.101	-0.028	-0.038						
0.2	-0.183	-0.188	-0.218	-0.197	-0.095						
0.2	0.017	0.082	0.058	0.077	0.118						
0.2	0.169	0.205	0.257	0.206	0.107						
0.3	0.183	0.225	0.257	0.205	0.121						

0.27	0.10	0.31	0.15	0.18
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.3	0.000	0.000	0.000	0.000

U VELOCITY FIELD						STEP NUMBER	1	TIME	12000.00	LEVEL	7
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.2	0.000	0.000	0.000	0.000	0.000						
0.2	0.000	0.000	0.000	0.000	0.000						
0.2	0.000	0.000	0.000	0.000	0.000						
0.2	0.000	0.000	0.000	0.000	0.000						
0.3	0.000	0.000	0.000	0.000	0.000						

MOVING GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF MOVING GRID IS AT X = 0.1780, Y = 0.2620 IN SCORERS WITH RESPECT TO THE CENTER OF THE PIPER UPPER BODY
 THE NEW GRID ORIGINATING IN THE MOVING SYSTEM IS 0.1264441 SCORERS IN X AND 0.0219410 SCORERS IN Y
 THE GRID DEFORMATION IN THE PIPER SYSTEM IS 0.016 SCORERS IN X AND 0.016 SCORERS IN Y

THE AVERAGE VALUES OF X, Y AND Z ARE 0.000007 0.078187 0.755151
 THE STANDARD DEVIATIONS ARE 0.000751 0.012580 3.182094

CONCENTRATION IN MC OF OIL PER ML OF WATER						STEP NUMBER	1	TIME	12000.00	LEVEL	1
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.10	0.00000	0.00000	0.00000	0.00000	0.00000						
0.21	0.00000	0.00000	0.00000	0.00000	0.00000						
0.23	0.00000	0.00000	0.00000	0.00000	0.00000						
0.25	0.00000	0.00000	0.00000	0.00000	0.00000						
0.26	0.00000	0.00000	0.00000	0.00000	0.00000						

CONCENTRATION IN MC OF OIL PER ML OF WATER						STEP NUMBER	1	TIME	12000.00	LEVEL	2
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.10	0.00000	0.00000	0.00000	0.00000	0.00000						
0.21	0.00000	0.00000	0.00000	0.00000	0.00000						
0.23	0.00000	0.00000	0.00000	0.00000	0.00000						
0.25	0.00000	0.00000	0.00000	0.00000	0.00000						
0.26	0.00000	0.00000	0.00000	0.00000	0.00000						

CONCENTRATION IN MC OF OIL PER ML OF WATER						STEP NUMBER	1	TIME	12000.00	LEVEL	3
U	V	W	X	Y	Z						
0.27	0.10	0.31	0.15	0.18							
0.10	0.00000	0.00000	0.00000	0.00000	0.00000						
0.21	0.00000	0.00000	0.00000	0.00000	0.00000						
0.23	0.00000	0.00000	0.00000	0.00000	0.00000						
0.25	0.00000	0.00000	0.00000	0.00000	0.00000						
0.26	0.00000	0.00000	0.00000	0.00000	0.00000						

Figure VIII.-7. Output from Main

PARTICLE POSITIONS X AND Y IN THE PLANTING SYSTEM IN DEGREES X IN METERS
 PARTICLE PARAMETERS AT TIME 12000.00

ID	PARTICLE POSITION PLANTING SYSTEM			PARTICLE POSITION PISTON SYSTEM			DENSITY	SPR. VPL.	RECS	
	X	Y	Z	X	Y	Z				
1	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.400
2	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.402
3	0.0027	0.0010	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.404
4	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.406
5	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.408
6	0.0025	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.410
7	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.412
8	0.0027	0.0020	0.1022	0.217	0.184	0.1022	0.0013	0.4770	0.0000	0.414
9	0.0028	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.416
10	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.418
11	0.0027	0.0020	0.1865	0.217	0.184	0.1865	0.0013	0.4770	0.0000	0.420
12	0.0027	0.0020	0.5072	0.217	0.184	0.5072	0.0010	0.4770	0.0000	0.422
13	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.424
14	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.426
15	0.0026	0.0020	0.1558	0.217	0.184	0.1558	0.0010	0.4770	0.0000	0.428
16	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.430
17	0.0026	0.0020	0.4167	0.217	0.184	0.4167	0.0010	0.4770	0.0000	0.432
18	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.434
19	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.436
20	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.438
21	0.0025	0.0010	0.4150	0.216	0.184	0.4150	0.0010	0.4770	0.0000	0.440
22	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.442
23	0.0027	0.0020	0.1918	0.217	0.184	0.1918	0.0010	0.4770	0.0000	0.444
24	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.446
25	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.448
26	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.450
27	0.0028	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.452
28	0.0027	0.0010	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.454
29	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.456
30	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.458
31	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.460
32	0.0027	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.462
33	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.464
34	0.0026	0.0020	0.1609	0.217	0.184	0.1609	0.0010	0.4770	0.0000	0.466
35	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.468
36	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0010	0.4770	0.0000	0.470
37	0.0027	0.0020	0.5030	0.217	0.184	0.5030	0.0013	0.4770	0.0000	0.472
38	0.0026	0.0020	0.4150	0.217	0.184	0.4150	0.0013	0.4770	0.0000	0.474
39	0.0015	0.0018	0.4150	0.215	0.187	0.4150	0.0013	0.4770	0.0000	0.476
40	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.478
41	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.480
42	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.482
43	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.484
44	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.486
45	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.488
46	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.490
47	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.492
48	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.494
49	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.496
50	0.0016	0.0017	0.4150	0.216	0.187	0.4150	0.0013	0.4770	0.0000	0.498

Figure VIII.-7. Output from Main

51	0.0007	0.0788	0.0150	0.210	0.117	0.0150	0.0011	1.0010	0.0000	1.001
52	0.0050	0.0621	0.0150	0.210	0.125	0.0150	0.0010	1.0010	0.0000	1.001
53	0.0070	0.0620	0.0150	0.221	0.176	0.0150	0.0011	1.0010	0.0000	1.001
54	0.0050	0.0620	0.0150	0.210	0.125	0.0150	0.0010	1.0010	0.0000	1.001
55	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
56	0.0016	0.0016	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
57	0.0020	0.0491	0.0150	0.215	0.117	0.0150	0.0010	1.0010	0.0000	0.000
58	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
59	0.0017	0.0490	0.0150	0.207	0.111	0.0150	0.0010	1.0010	0.0000	0.000
60	0.0052	0.0610	0.0150	0.220	0.125	0.0150	0.0010	1.0010	0.0000	0.000
61	0.0017	0.0621	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
62	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
63	0.0010	0.0497	0.0150	0.210	0.122	0.0150	0.0010	1.0010	0.0000	0.000
64	0.0000	0.0621	0.0150	0.210	0.125	0.0150	0.0010	1.0010	0.0000	0.000
65	0.0052	0.0614	0.0150	0.210	0.126	0.0150	0.0010	1.0010	0.0000	0.000
66	0.0070	0.0622	0.0150	0.221	0.176	0.0150	0.0011	1.0010	0.0000	0.000
67	0.0016	0.0016	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
68	0.0007	0.0610	0.0150	0.210	0.106	0.0150	0.0010	1.0010	0.0000	0.000
69	0.0006	0.0600	0.0150	0.221	0.127	0.0150	0.0010	1.0010	0.0000	0.000
70	0.0007	0.0602	0.0150	0.210	0.127	0.0150	0.0010	1.0010	0.0000	0.000
71	0.0016	0.0614	0.0150	0.221	0.176	0.0150	0.0010	1.0010	0.0000	0.000
72	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
73	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
74	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
75	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
76	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
77	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
78	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
79	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
80	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
81	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
82	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
83	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
84	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
85	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
86	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
87	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
88	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
89	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
90	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
91	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
92	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
93	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
94	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
95	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
96	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
97	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
98	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
99	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
100	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
101	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000
102	0.0016	0.0017	0.0150	0.216	0.107	0.0150	0.0010	1.0010	0.0000	0.000

DATA SUMMARY

TOTAL MASS OF ALL PARTICLES 2000.0000 0000.0000

FORMATION OF OIL	NUMBER (PARTS PER MIL)	PERCENT OF TOTAL
IN SYSTEM	1016.72200	50.80
ON SURFACE	1000.00000	50.00
IN WATER COLUMN	100.00000	5.00
ON SURFACE	100.00000	5.00
ON SURFACE	0.00000	0.00
SPECIAL REFERENCES		
MINORITIES FORMING	0.00000	0.00
PARTICULARS FORMING	0.00000	0.00
LAST YEAR APP. APPROX.	0.00000	0.00

Figure VIII.-7. Output from Main

SPILL CONTROL PARAMETERS 12,000 HOURS AFTER THE BEGINNING OF THE SPILL.
 GOVERNORIAL DATA FROM THIS STEP: 0000
 NUMBER OF SPILLS OF SPILL CONTROL REPORTS THIS STEP: 0 SPILLS: 1 CLEANUP REPORTS: 0 RECOVERY REPORTS.

CRITICAL CLEANUP REPORTS IN PROGRESS 12,00000 HOURS AFTER THE BEGINNING OF THIS STEP
 AND CLEANUP REPORTS THIS TIME STEP
 THE 1 CLEANUP REPORT CURRENTLY UNDERWAY IS CENTERED AT LONGITUDE 44.77000 AND LATITUDE 41.61000
 THE RADIUS OF COVERAGE OF THIS REPORT IS 10000.000 METERS
 THE CLEANUP RATE OF RECOVERY IS 100.00000 TONS/HOUR WITH AN EFFICIENCY OF 90.00000
 THIS CLEANUP STARTS 12.00000 HOURS AFTER THE BEGINNING OF THE SPILL AND LASTS 1.00000 HOURS

PLANKING SPILLS 12,000 HOURS AFTER THE BEGINNING OF THE SPILL
 SPILLS CURRENTLY BEING TO THIS STEP
 THE 1 SPILL APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 44.78010 AND LATITUDE 41.42100,
 IS OF RADIUS 1690.98 METERS AND IS OF WEIGHT 7189.8710 TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.01181 GRAMS/CC
 INTERFACIAL TENSION 10.00000 DYNES/CM
 KINEMATIC VISCOSITY 1.00000 CENTISTOKES
 BY WEIGHT THE OIL FRACTIONS ARE:

PETROLEUM (C4-C12)	0.001065
PETROLEUM (C13-C22)	0.004900
CYCLOHEXANNE (C6-C12)	0.001845
CYCLOHEXANNE (C13-C22)	0.000005
AROMATIC (C4-C12)	0.002365
AROMATIC (C13-C18)	3.073487
AROMATIC-AROMATIC (C9-C25)	0.709177
RESIDUAL	0.300000

THE 2 SPILL APPEARED 1.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 44.78010 AND LATITUDE 41.42000,
 IS OF RADIUS 1692.48 METERS AND IS OF WEIGHT 7617.0900 TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.01181 GRAMS/CC
 INTERFACIAL TENSION 10.00000 DYNES/CM
 KINEMATIC VISCOSITY 1.00000 CENTISTOKES
 BY WEIGHT THE OIL FRACTIONS ARE:

PETROLEUM (C4-C12)	0.001065
PETROLEUM (C13-C22)	0.004900
CYCLOHEXANNE (C6-C12)	0.001845
CYCLOHEXANNE (C13-C22)	0.000005
AROMATIC (C4-C12)	3.073487
AROMATIC (C13-C18)	0.002365
AROMATIC-AROMATIC (C9-C25)	0.709177
RESIDUAL	0.300000

AMOUNT OF OIL PHYSICALLY RECOVERED FROM THE 1 SPILL AT 12,000 HOURS AFTER THE BEGINNING OF THE SPILL IS 100.00000 TONS
 AMOUNT OF OIL PHYSICALLY RECOVERED FROM THE 2 SPILL AT 12,000 HOURS AFTER THE BEGINNING OF THE SPILL IS 100.00000 TONS

PLANKING GRID DEFINITION AND STATISTICAL LOCATION STATISTICS
 ORDER OF PLANKING GRID IS AT X 0.1641, Y 0.2629 IN DEGREES WITH RESPECT TO THE CENTER OF THE SPILL
 THE GRID SEPARATION IN THE PLANKING SYSTEM IS 0.074772 DEGREES IN X AND 0.071810 DEGREES IN Y
 THE GRID SEPARATION IN THE SPILL SYSTEM IS 0.036 DEGREES IN X AND 0.035 DEGREES IN Y
 THE STANDARD DEVIATION OF X, Y AND Z ARE 0.055661, 0.072400, 0.720200
 THE STANDARD DEVIATIONS ARE 0.011017, 0.011010, 0.863350
 HORIZONTAL X-Y SCALE DEPENDENCY DIFFUSION COEFF. 0.00000-05, 0.14519-36
 XAVG= 0.5819-01, YAVG= 0.1377-01, ZAVG= 0.758, XSTD= 0.0458-024107, YSTD= 0.1239-01

Figure VIII.-7. Output from Main

ALL HORIZONTAL VELOCITIES AND MULTIPLIERS BY 10000

U VELOCITY FIELD						V VELOCITY FIELD						W VELOCITY FIELD					
U		V		W		U		V		W		U		V		W	
0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17
0.2	-0.181	-0.170	-0.066	0.007	-0.031	0.2	-0.181	-0.170	-0.066	0.007	-0.031	0.2	-0.181	-0.170	-0.066	0.007	-0.031
0.2	-0.127	-0.180	-0.198	-0.174	-0.081	0.2	-0.127	-0.180	-0.198	-0.174	-0.081	0.2	-0.127	-0.180	-0.198	-0.174	-0.081
0.2	0.118	0.187	0.177	0.195	0.233	0.2	0.118	0.187	0.177	0.195	0.233	0.2	0.118	0.187	0.177	0.195	0.233
0.1	0.188	0.270	0.252	0.288	0.310	0.1	0.188	0.270	0.252	0.288	0.310	0.1	0.188	0.270	0.252	0.288	0.310
0.1	0.284	0.298	0.108	0.128	0.169	0.1	0.284	0.298	0.108	0.128	0.169	0.1	0.284	0.298	0.108	0.128	0.169

U VELOCITY FIELD						V VELOCITY FIELD						W VELOCITY FIELD					
U		V		W		U		V		W		U		V		W	
0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17
0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000	0.2	0.000	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000	0.000	0.1	0.000	0.000	0.000	0.000	0.000	0.1	0.000	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000	0.000	0.1	0.000	0.000	0.000	0.000	0.000	0.1	0.000	0.000	0.000	0.000	0.000

MOVING GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1410, 0.7487) IN DEGREE WITH RESPECT TO THE POINTS OF THE PEEP DEPTH GRID
 THE SP GRID SEPARATION IN THE FLOATING SYSTEM IS 0.021187 DEGREE IN X AND 0.021187 DEGREE IN Y
 THE GRID SEPARATION IN THE PEEP SYSTEM IS 0.036 DEGREE IN X AND 0.036 DEGREE IN Y
 THE AVERAGE VALUES OF X, Y AND Z ARE 0.06617 0.071766 0.761937
 THE STANDARD DEVIATIONS ARE 0.010686 0.012585 0.182887

CONCENTRATION IN % OF OIL PER ML OF WATER						CONCENTRATION IN % OF OIL PER ML OF WATER						CONCENTRATION IN % OF OIL PER ML OF WATER					
U		V		W		U		V		W		U		V		W	
0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17	0.27	0.10	0.32	0.15	0.17	0.17
0.18	0.0000	0.0000	0.0000	0.0000	0.0000	0.18	0.0000	0.0000	0.0000	0.0000	0.0000	0.18	0.0000	0.0000	0.0000	0.0000	0.0000
0.21	0.0000	0.0000	0.0000	0.0000	0.0000	0.21	0.0000	0.0000	0.0000	0.0000	0.0000	0.21	0.0000	0.0000	0.0000	0.0000	0.0000
0.23	0.0000	0.0000	0.0000	0.0000	0.0000	0.23	0.0000	0.0000	0.0000	0.0000	0.0000	0.23	0.0000	0.0000	0.0000	0.0000	0.0000
0.24	0.0000	0.0000	0.0000	0.0000	0.0000	0.24	0.0000	0.0000	0.0000	0.0000	0.0000	0.24	0.0000	0.0000	0.0000	0.0000	0.0000

Figure VIII.-7. Output from Main

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IN DROPPS X IN 40 PPM
 PARTICLE PARAMETER AT TIME 0.1700,00

N	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION PIPE SYSTEM			DENSITY	DENSITY	SP. VOL.	RHO
	X	Y	Z	X	Y	Z				
1	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
2	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
3	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
4	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
5	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
6	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
7	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
8	0.0510	0.0020	0.1022	0.215	0.101	0.1022	0.0013	0.0770	0.0000	0.000
9	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
10	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
11	0.0510	0.0020	0.1065	0.215	0.101	0.1065	0.0013	0.0770	0.0000	0.000
12	0.0510	0.0020	0.5072	0.215	0.101	0.5072	0.0013	0.0770	0.0000	0.000
13	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
14	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
15	0.0510	0.0020	0.1558	0.215	0.101	0.1558	0.0013	0.0770	0.0000	0.000
16	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
17	0.0510	0.0020	0.0167	0.215	0.101	0.0167	0.0013	0.0770	0.0000	0.000
18	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
19	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
20	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
21	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
22	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
23	0.0510	0.0020	0.1018	0.215	0.101	0.1018	0.0013	0.0770	0.0000	0.000
24	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
25	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
26	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
27	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
28	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
29	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
30	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
31	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
32	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
33	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
34	0.0510	0.0020	0.1600	0.215	0.101	0.1600	0.0013	0.0770	0.0000	0.000
35	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
36	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
37	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
38	0.0510	0.0020	0.0150	0.215	0.101	0.0150	0.0013	0.0770	0.0000	0.000
39	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
40	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
41	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
42	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
43	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
44	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
45	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
46	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
47	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
48	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
49	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000
50	0.0509	0.0017	0.0150	0.210	0.102	0.0150	0.0013	0.0770	0.0000	0.000

Figure VIII.-7. Output from Main

1	0.0510	0.0769	0.8150	0.217	0.111	0.8150	0.0013	1.0013	0.0000	1.001
2	0.0505	0.0621	0.8150	0.217	0.120	0.8150	0.0010	1.0010	0.0000	1.001
3	0.0548	0.0627	0.8150	0.220	0.111	0.8150	0.0013	1.0013	0.0000	1.001
4	0.0540	0.0672	0.8150	0.217	0.120	0.8150	0.0013	1.0013	0.0000	1.001
5	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0013	0.8770	0.0000	0.981
6	0.0500	0.0016	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
7	0.0510	0.0000	0.8150	0.215	0.117	0.8150	0.0010	1.0010	0.0000	1.001
8	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0013	0.8770	0.0000	0.980
9	0.0662	0.0642	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	1.001
10	0.0550	0.0614	0.8150	0.218	0.120	0.8150	0.0013	1.0013	0.0000	1.001
11	0.0010	0.0615	0.8150	0.200	0.120	0.8150	0.0010	1.0010	0.0000	1.001
12	0.0000	0.0017	0.8150	0.218	0.102	0.8150	0.0013	0.8770	0.0000	0.980
13	0.0520	0.0505	0.8150	0.216	0.117	0.8150	0.0010	1.0010	0.0000	1.001
14	0.0713	0.0620	0.8150	0.218	0.121	0.8150	0.0010	1.0010	0.0000	1.001
15	0.0502	0.0613	0.8150	0.217	0.120	0.8150	0.0010	1.0010	0.0000	1.001
16	0.0547	0.0502	0.8150	0.220	0.117	0.8150	0.0010	1.0010	0.0000	1.001
17	0.0500	0.0016	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
18	0.0550	0.0610	0.8150	0.210	0.122	0.8150	0.0010	1.0010	0.0000	1.001
19	0.0517	0.0500	0.8150	0.217	0.117	0.8150	0.0010	1.0010	0.0000	1.001
20	0.0540	0.0610	0.8150	0.220	0.122	0.8150	0.0013	1.0013	0.0000	1.001
21	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
22	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
23	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0013	0.8770	0.0000	0.980
24	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
25	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
26	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
27	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
28	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
29	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
30	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
31	0.0510	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
32	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0013	0.8770	0.0000	0.980
33	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
34	0.0517	0.0651	0.8150	0.216	0.121	0.8150	0.0010	0.8770	0.0000	0.980
35	0.0601	0.0150	0.8150	0.217	0.200	0.8150	0.0010	1.0010	0.0000	1.000
36	0.0507	0.0005	0.8150	0.222	0.105	0.8150	0.0013	1.0013	0.0000	1.000
37	0.0565	0.0007	0.8150	0.210	0.105	0.8150	0.0013	1.0013	0.0000	1.001
38	0.0517	0.0010	0.8150	0.216	0.100	0.8150	0.0010	1.0010	0.0000	1.000
39	0.0617	0.0670	0.8150	0.227	0.126	0.8150	0.0013	0.8952	0.0000	0.950
40	0.0516	0.0000	0.8150	0.217	0.201	0.8150	0.0013	1.0013	0.0000	1.000
41	0.0500	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
42	0.0510	0.0017	0.8150	0.218	0.102	0.8150	0.0010	0.8770	0.0000	0.980
43	0.0573	0.0710	0.8150	0.220	0.120	0.8150	0.0010	0.8952	0.0000	0.950
44	0.0507	0.0600	0.8150	0.210	0.127	0.8150	0.0013	0.8952	0.0000	0.950
45	0.0505	0.0510	0.8150	0.210	0.110	0.8150	0.0013	1.0013	0.0000	0.981
46	0.0607	0.0607	0.8150	0.211	0.117	0.8150	0.0010	1.0010	0.0000	0.981
47	0.0607	0.0511	0.8150	0.200	0.117	0.8150	0.0013	1.0013	0.0000	0.980
48	0.0500	0.0005	0.8150	0.201	0.100	0.8150	0.0010	1.0010	0.0000	0.980
49	0.0505	0.0670	0.8150	0.211	0.126	0.8150	0.0010	1.0010	0.0000	0.981
100	0.0500	0.0711	0.8150	0.222	0.120	0.8150	0.0010	1.0010	0.0000	0.981
101	0.0700	0.0670	0.8150	0.211	0.126	0.8150	0.0010	1.0010	0.0000	0.981
102	0.0600	0.0670	0.8150	0.211	0.126	0.8150	0.0010	1.0010	0.0000	0.981
103	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981
104	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981
105	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981
106	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981
107	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981
108	0.0500	0.0670	0.8150	0.200	0.127	0.8150	0.0010	1.0010	0.0000	0.981

DATA SUMMARY

TOTAL MASS OF ALL PARTICLES 2000.0000 0.0000

LOCATION OF PARTICLE	NUMBER (TOTAL MASS)	PERCENT OF TOTAL
IN STRONGEST	8017.0000	20.00
ON SURFACE	10271.0000	71.17
IN WATER COLUMN	100.0000	0.11
ON BOTTOM	81.0000	0.11
ON CRACK	0.0000	0.00
SPECIAL PROCESSES		
BIOLOGICALLY CONSUMED	0.0000	0.00
TRISTICALLY CLIPPED UP	500.0000	1.00
LOST THROUGH ANCHORAGE	0.0000	0.00
LOST PARTICLES		

Figure VIII.-7. Output from Main

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DRILL CONTROL PARAMETERS 15,000 HOURS AFTER THE BEGINNING OF THE DRILL
 PERIODICITY DATA FOR THIS STEP: none
 AMOUNT OF SPILLAGE IN DRILL CONTROL REPORTS THIS STEP: 1 SPILLAGE; 0 CLEANUP REPORTS; 0 TREATMENT REPORTS.

CRITICAL CLEANUP REPORTS IN PROGRESS 15,0000 HOURS AFTER THE BEGINNING OF THE DRILL
 CONTINUING DRILL CLEANUP REPORTS THIS STEP
 THE 1 CLEANUP REPORT CORRECTLY INITIATED IS CONTROLLED BY LONGITUDE 44.770000 AND LATITUDE 01.610000
 THE RANGE OF COVERAGE OF THIS REPORT IS 10000.000 METERS
 THE RELEASE RATE OF RECOVERY IS 100.000000 TONS/HOUR WITH AN EFFICIENCY OF 50.000000
 THIS CLEANUP STARTS 12,000000 HOURS AFTER THE BEGINNING OF THE DRILL AND LASTS 1,000110 HOURS

ENDING SPILLAGE 15,000 HOURS AFTER THE BEGINNING OF THE DRILL
 SPILLAGE CREATED PRIOR TO THIS STEP

THE 1 SPILLAGE APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE DRILL
 IT IS CONTROLLED BY LONGITUDE 44.774320 AND LATITUDE 01.627320
 IS OF RANGE 1844.21 METERS AND IS OF WEIGHT 7420.1010 METERS TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.016900 G/CM³
 INTERFACIAL TENSION 10.000000 DYNES/CM
 SURFACTANT CONCENTRATION 1.000000 PERCENTAGE
 BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.333722
PARAFFIN (C11-C22)	0.094978
CYCLOPARAFFIN (C6-C12)	0.002757
CYCLOPARAFFIN (C11-C22)	0.000000
AROMATIC (C6-C11)	0.053118
AROMATIC (C12-C18)	0.070817
ANTHRACENE-AROMATIC (C9-C25)	0.208517
RESIDUAL	0.103710

THE 2 SPILLAGE APPEARED 1.00 HOURS AFTER THE BEGINNING OF THE DRILL
 IT IS CONTROLLED BY LONGITUDE 44.770000 AND LATITUDE 01.400110
 IS OF RANGE 1844.21 METERS AND IS OF WEIGHT 7420.1010 METERS TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.016900 G/CM³
 INTERFACIAL TENSION 10.000000 DYNES/CM
 SURFACTANT CONCENTRATION 1.000000 PERCENTAGE
 BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.330800
PARAFFIN (C11-C22)	0.094978
CYCLOPARAFFIN (C6-C12)	0.011678
CYCLOPARAFFIN (C11-C22)	0.000000
AROMATIC (C6-C11)	0.053118
AROMATIC (C12-C18)	0.070817
ANTHRACENE-AROMATIC (C9-C25)	0.208517
RESIDUAL	0.103710

HORIZONTAL E-Y SCALE APPROPRIATE DISPERSION COEFF. = 0.1240E-04 0.2667E-04
 YAWD= 0.422E-01 YAWD= 0.147E-01 YAWD= 0.355 SIZD= 0.407E-03 SIZD= 0.124E-01

URING THE 1ST STEP WHICH BEGAN AT 15,000000 HOURS 100,00000 TONS OF OIL WERE PRESENTLY SPILLED FROM THE 1 DRILL
 DURING THE 2ND STEP WHICH BEGAN AT 15,000000 HOURS 100,00000 TONS OF OIL WERE PRESENTLY SPILLED FROM THE 2 DRILL

FLOATING GRID DEFINITION AND PARTICLE LOCATION SUBROUTINE

ORIGIN OF FLOATING GRID IS AT X 0.15555 0.25401 IN METERS WITH RESPECT TO THE CENTER OF THE PIPELINES GRID
 THE NEW GRID COORDINATE IN THE FLOATING SYSTEM IS 0.0132150 METERS IN X AND 1.0210112 METERS IN Y
 THE GRID COORDINATE IN THE PIPELINES SYSTEM IS 0.016 METERS IN X AND 0.015 METERS IN Y
 THE APPROX VALUES OF X, Y AND Z ARE 0.06700 0.071021 0.735017
 THE STANDARD DEVIATIONS ARE 0.014517 0.014607 0.022003
 HORIZONTAL E-Y SCALE APPROPRIATE DISPERSION COEFF. = 0.5410E-04 0.4781E-04
 YAWD= 0.648E-01 YAWD= 0.726E-01 YAWD= 0.354 SIZD= 0.117E-03 SIZD= 0.117E-01

Figure VIII.-7. Output from Main

ALL HORIZONTAL VELOCITIES ARE MULTIPLIED BY 10000

U VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	-0.161	-0.092	-0.092	0.027	-0.027					
0.2	-0.122	-0.168	-0.127	-0.152	-0.070					
0.2	0.157	0.198	0.211	0.202	0.200					
0.3	0.195	0.211	0.286	0.201	0.115					
0.1	0.185	0.177	0.406	0.478	0.450					

U VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	2
0.27	0.20	0.12	0.18	0.17						
0.2	-0.161	-0.092	-0.092	0.027	-0.027					
0.2	-0.122	-0.168	-0.127	-0.152	-0.070					
0.2	0.157	0.198	0.211	0.202	0.200					
0.1	0.195	0.211	0.286	0.201	0.115					
0.3	0.185	0.177	0.406	0.478	0.450					

U VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	-0.151	-0.092	-0.092	0.027	-0.027					
0.2	-0.122	-0.168	-0.127	-0.152	-0.070					
0.2	0.157	0.198	0.211	0.202	0.200					
0.3	0.195	0.211	0.286	0.201	0.115					
0.1	0.185	0.177	0.406	0.478	0.450					

V VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	-0.466	-0.482	-0.495	-0.510	-0.520					
0.2	-0.471	-0.520	-0.510	-0.411	-0.191					
0.2	-0.290	-0.185	-0.172	-0.167	-0.120					
0.3	-0.104	-0.252	-0.261	-0.215	-0.217					
0.3	-0.112	-0.112	-0.272	-0.170	-0.129					

V VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	2
0.27	0.20	0.12	0.18	0.17						
0.2	-0.456	-0.492	-0.495	-0.510	-0.520					
0.2	-0.471	-0.520	-0.510	-0.411	-0.191					
0.2	-0.290	-0.185	-0.172	-0.167	-0.120					
0.3	-0.104	-0.252	-0.261	-0.215	-0.217					
0.3	-0.112	-0.112	-0.272	-0.170	-0.129					

V VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	-0.466	-0.482	-0.495	-0.510	-0.520					
0.2	-0.471	-0.520	-0.510	-0.411	-0.191					
0.2	-0.290	-0.185	-0.172	-0.167	-0.120					
0.3	-0.104	-0.252	-0.261	-0.215	-0.217					
0.3	-0.112	-0.112	-0.272	-0.170	-0.129					

W VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.3	0.000	0.000	0.000	0.000	0.000					
0.1	0.000	0.000	0.000	0.000	0.000					

W VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	2
0.27	0.20	0.12	0.18	0.17						
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.3	0.000	0.000	0.000	0.000	0.000					
0.1	0.000	0.000	0.000	0.000	0.000					

W VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.3	0.000	0.000	0.000	0.000	0.000					
0.1	0.000	0.000	0.000	0.000	0.000					

0.27	0.20	0.12	0.18	0.17
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000
0.3	0.000	0.000	0.000	0.000
0.1	0.000	0.000	0.000	0.000

W VELOCITY FIELD					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.2	0.000	0.000	0.000	0.000	0.000					
0.1	0.000	0.000	0.000	0.000	0.000					
0.3	0.000	0.000	0.000	0.000	0.000					

LOADING GRID DEFINITION AND CHECKED LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1516, 0.2718) IN MDCAPPS WITH RESPECT TO THE ORIGIN OF THE FIXED OPPER GRID
 THE NEW GRID ORIGIN IN THE FLOATING SYSTEM IS 0.018465 MDCAPPS IN X AND 1.0218078 MDCAPPS IN Y
 THE GRID ORIGIN IN THE FIXED SYSTEM IS 0.018 MDCAPPS IN X AND 0.018 MDCAPPS IN Y

THE APPROX VALUES OF X, Y AND Z ARE 0.064912 0.072529 0.758116
 THE STANDARD DEVIATIONS ARE 0.018911 0.018102 0.181884

CONCENTRATION IN MG OF OIL PER ML OF WATER					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.17	0.00000	0.00000	0.00000	0.00000	0.00000					
0.20	0.00000	0.00000	0.00019	0.00047	0.00000					
0.24	0.00000	0.00000	0.00028	0.00048	0.00000					
0.27	0.00000	0.00000	0.00005	0.00004	0.00000					
0.10	0.00000	0.00000	0.00000	0.00000	0.00000					

CONCENTRATION IN MG OF OIL PER ML OF WATER					STEP NUMBER	%	TIME	50000.00	LEVEL	2
0.27	0.20	0.12	0.18	0.17						
0.17	0.00000	0.00000	0.00000	0.00000	0.00000					
0.20	0.00000	0.00009	0.00019	0.00055	0.00000					
0.24	0.00000	0.00012	0.00112	0.00168	0.00000					
0.27	0.00000	0.00008	0.00028	0.00028	0.00000					
0.10	0.00000	0.00000	0.00000	0.00000	0.00000					

CONCENTRATION IN MG OF OIL PER ML OF WATER					STEP NUMBER	%	TIME	50000.00	LEVEL	1
0.27	0.20	0.12	0.18	0.17						
0.17	0.00000	0.00000	0.00000	0.00000	0.00000					
0.20	0.00000	0.00120	0.00552	0.01896	0.00000					
0.24	0.00000	0.00111	0.00529	0.00714	0.00000					
0.27	0.00000	0.00055	0.00168	0.00051	0.00000					
0.10	0.00000	0.00000	0.00000	0.00000	0.00000					

Figure VIII.-7. Output from Main

PARTICLE POSITIONS Y AND Z IN THE FLOATING SYSTEM IN DEGREES X IN NEUTRONS
 PARTICLE PARAMETERS AT TIME 50000.00

#	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION FIXED SYSTEM			DISTANCE	DENSITY	SP. VEL.	RATE
	X	Y	Z	X	Y	Z				
1	0.0618	0.0826	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
2	0.0619	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
3	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
4	0.0619	0.0827	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
5	0.0518	0.0825	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
6	0.0618	0.0825	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
7	0.0519	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
8	0.0619	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
9	0.0520	0.0825	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
10	0.0619	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
11	0.0619	0.0825	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
12	0.0619	0.0825	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
13	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
14	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
15	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
16	0.0519	0.0826	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
17	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
18	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
19	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
20	0.0519	0.0826	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
21	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
22	0.0518	0.0826	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
23	0.0619	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
24	0.0519	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
25	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
26	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
27	0.0620	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
28	0.0519	0.0827	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
29	0.0619	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
30	0.0519	0.0825	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
31	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
32	0.0519	0.0825	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
33	0.0620	0.0825	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
34	0.0518	0.0825	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
35	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
36	0.0519	0.0826	0.8150	0.213	0.116	0.8150	0.0010	0.8770	0.0000	0.999
37	0.0619	0.0826	0.8150	0.210	0.116	0.8150	0.0010	0.8770	0.0000	0.999
38	0.0618	0.0826	0.8150	0.211	0.116	0.8150	0.0010	0.8770	0.0000	0.999
39	0.0600	0.0818	0.8150	0.212	0.117	0.8150	0.0010	0.8770	0.0000	0.999
40	0.0519	0.0818	0.8150	0.213	0.117	0.8150	0.0010	0.8770	0.0000	0.999
41	0.0610	0.0818	0.8150	0.211	0.117	0.8150	0.0010	0.8770	0.0000	0.999
42	0.0510	0.0818	0.8150	0.213	0.117	0.8150	0.0010	0.8770	0.0000	0.999
43	0.0600	0.0827	0.8150	0.216	0.116	0.8150	0.0010	0.8770	0.0000	1.001
44	0.0710	0.0600	0.8150	0.225	0.122	0.8150	0.0010	1.0010	0.0000	1.001
45	0.0610	0.0600	0.8150	0.211	0.117	0.8150	0.0010	0.8770	0.0000	0.999
46	0.0511	0.0600	0.8150	0.205	0.121	0.8150	0.0010	1.0010	0.0000	1.001
47	0.0610	0.0618	0.8150	0.211	0.117	0.8150	0.0010	0.8770	0.0000	0.999
48	0.0511	0.0618	0.8150	0.213	0.117	0.8150	0.0010	0.8770	0.0000	0.999
49	0.0711	0.0511	0.8150	0.203	0.107	0.8150	0.0010	1.0010	0.0000	1.001
50	0.0607	0.0607	0.8150	0.210	0.116	0.8150	0.0010	1.0010	0.0000	1.001

Figure VIII.-7. Output from Main

51	0.0617	0.0701	0.0150	0.215	0.128	0.0150	0.0011	1.3112	0.0000	1.001
52	0.0615	0.0617	0.0150	0.216	0.115	0.0150	2.0010	1.0012	0.0000	1.001
53	0.0617	0.0618	0.0150	0.218	0.116	0.0150	0.0010	1.0112	0.0000	1.001
54	0.0608	0.0618	0.0150	0.216	0.116	0.0150	0.0112	1.0012	0.0000	1.001
55	0.0610	0.0610	0.0150	0.211	0.117	0.0150	3.0010	1.0112	0.0000	0.998
56	0.0610	0.0611	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
57	0.0610	0.0608	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	1.001
58	0.0608	0.0701	0.0150	0.211	0.128	0.0150	3.0010	1.0112	0.0000	1.001
59	0.0610	0.0618	0.0150	0.217	0.116	0.0150	0.0010	1.0112	0.0000	1.001
60	0.0616	0.0608	0.0150	0.201	0.116	0.0150	0.0010	1.0012	0.0000	1.001
61	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
62	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
63	0.0628	0.0600	0.0150	0.210	0.112	0.0150	3.0010	1.0012	0.0000	1.001
64	0.0610	0.0612	0.0150	0.215	0.117	0.0150	0.0010	1.0112	0.0000	1.001
65	0.0602	0.0600	0.0150	0.216	0.115	0.0150	0.0010	1.0012	0.0000	1.001
66	0.0617	0.0600	0.0150	0.210	0.113	0.0150	0.0010	1.0012	0.0000	1.001
67	0.0610	0.0611	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
68	0.0616	0.0600	0.0150	0.215	0.115	0.0150	0.0010	1.0012	0.0000	1.001
69	0.0618	0.0615	0.0150	0.217	0.117	0.0150	0.0010	1.0012	0.0000	1.001
70	0.0617	0.0605	0.0150	0.215	0.112	0.0150	0.0010	1.3112	0.0000	1.001
71	0.0608	0.0611	0.0150	0.210	0.117	0.0150	3.0010	1.0012	0.0000	1.001
72	0.0608	0.0610	0.0150	0.212	0.117	0.0150	0.0010	0.0112	0.0000	0.998
73	0.0609	0.0610	0.0150	0.212	0.117	0.0150	0.0010	0.0112	0.0000	0.998
74	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
75	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
76	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
77	0.0609	0.0610	0.0150	0.212	0.117	0.0150	0.0010	0.0112	0.0000	0.998
78	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
79	0.0609	0.0611	0.0150	0.211	0.117	0.0150	3.0010	1.0112	0.0000	0.998
80	0.0609	0.0611	0.0150	0.212	0.117	0.0150	0.0010	0.0112	0.0000	0.998
81	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
82	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
83	0.0610	0.0610	0.0150	0.211	0.117	0.0150	0.0010	0.0112	0.0000	0.998
84	0.0617	0.0608	0.0150	0.215	0.118	0.0150	0.0010	0.0112	0.0000	0.998
85	0.0610	0.0608	0.0150	0.215	0.117	0.0150	0.0010	1.0012	0.0000	1.000
86	0.0606	0.0608	0.0150	0.220	0.100	0.0150	0.0010	1.0012	0.0000	1.000
87	0.0602	0.0608	0.0150	0.210	0.100	0.0150	0.0010	1.0012	0.0000	1.000
88	0.0610	0.0611	0.0150	0.205	0.100	0.0150	0.0010	1.0012	0.0000	1.000
89	0.0608	0.0610	0.0150	0.226	0.101	0.0150	0.0010	0.0112	0.0000	0.998
90	0.0611	0.0608	0.0150	0.215	0.100	0.0150	0.0010	1.0112	0.0000	1.000
91	0.0607	0.0610	0.0150	0.212	0.110	0.0150	3.0010	1.0012	0.0000	0.998
92	0.0610	0.0600	0.0150	0.215	0.101	0.0150	0.0010	0.0112	0.0000	0.998
93	0.0611	0.0707	0.0150	0.210	0.125	0.0150	0.0010	0.0112	0.0000	0.998
94	0.0608	0.0608	0.0150	0.210	0.121	0.0150	0.0010	0.0112	0.0000	0.998
95	0.0600	0.0510	0.0150	0.216	0.105	0.0150	3.0010	1.0102	0.0000	0.998
96	0.0611	0.0600	0.0150	0.211	0.108	0.0150	0.0010	1.0012	0.0000	0.998
97	0.0600	0.0500	0.0150	0.251	0.100	0.0150	0.0010	1.3112	0.0000	0.998
98	0.0720	0.0600	0.0150	0.200	0.100	0.0150	0.0010	1.0102	0.0000	0.998
99	0.0620	0.0617	0.0150	0.210	0.121	0.0150	3.0010	1.0012	0.0000	0.998
100	0.0600	0.0700	0.0150	0.221	0.115	0.0150	0.0010	1.0012	0.0000	0.998
101	0.0620	0.0617	0.0150	0.210	0.121	0.0150	0.0010	1.3112	0.0000	0.998
102	0.0610	0.0617	0.0150	0.211	0.121	0.0150	0.0010	1.0012	0.0000	0.998
103	0.0735	0.0617	0.0150	0.261	0.110	0.0150	0.0010	1.0012	0.0000	0.998
104	0.0717	0.0712	0.0150	0.250	0.111	0.0150	0.0010	1.0010	0.0000	0.998
105	0.0950	0.0811	0.0150	0.207	0.101	0.0150	0.0010	1.1112	0.0000	1.000
106	0.0717	0.0611	0.0150	0.250	0.115	0.0150	3.0010	1.0112	0.0000	1.000
107	0.0617	0.0618	0.0150	0.200	0.117	0.0150	0.0010	1.0110	0.0000	0.998
108	0.0610	0.0605	0.0150	0.210	0.108	0.0150	0.0010	1.0010	0.0000	0.998
109	0.0610	0.0611	0.0150	0.210	0.115	0.0150	0.0010	1.3312	0.0000	1.011
110	0.0600	0.0600	0.0150	0.210	0.110	0.0150	3.0010	1.0010	0.0000	1.011
111	0.0606	0.0605	0.0150	0.252	0.200	0.0150	0.0010	1.0112	0.0000	0.998
112	0.0602	0.0610	0.0150	0.271	0.206	0.0150	0.0010	1.0112	0.0000	0.998
113	0.0600	0.0606	0.0150	0.260	0.122	0.0150	3.0010	1.0000	0.0000	1.011
114	0.0606	0.0601	0.0150	0.282	0.101	0.0150	3.0010	1.0112	0.0000	0.998
115	0.0605	0.0616	0.0150	0.251	0.117	0.0150	0.0010	1.0000	0.0000	1.011

BASE BALANCE

TOTAL MASS OF OIL SPILLED 20000.0000 PPMIC TONS

LOCATION OF OIL IN STRONGBOX OR COMPART OR BAY OR BOTTLE OR CASE	AMOUNT (METRIC TONS)	PERCENT OF TOTAL
IN STRONGBOX	5001.2000	25.02
OR COMPART	1155.8000	5.78
OR BAY	110.0000	0.55
OR BOTTLE	45.4575	0.23
OR CASE	0.0000	0.00
APPROX RECALCULATED		
BIOLOGICALLY CONCERNED	0.03023	0.00
PHYSICALLY CLARIFIED OR LOST UPON OIL REMOVAL	1700.0000	8.50
LOST UPON OIL REMOVAL	0.00000	0.00

Figure VIII.-7. Output from Main

* * THIS IS A RESTARTED RUN * * *

INPUT CONTROL PARAMETERS		INPUT STREAM FOR THE SUBSURFACE PORTION OF THE MODEL		P AD JUNCTION		1 CONCENTRATION	7 PARTICLE	7 SPILLAGE END	7 HAS: DATA SETS FOR	7 STEPS
1	RSTRT			0.0000	10PILLETS					
1	RCTPR	1.11100	DRSE	10000.00000	25PILLETS					
1	RSURM	1.11100	DRSE	21600.00000	25PILLETS					
0	RSHW	0.05000	FEI	32400.00000	25PILLETS					
350	IDAT	0.05000	FEI	43200.00000	25PILLETS					
1	RFRV	0	STARS	54000.00000	25PILLETS					
3.00000	DT	10.00000	DE	64800.00000	25PILLETS					
11.00000	TIHAI	10.00000	DE			0.000	BEAD IN			
2	ISCLL	0.00001	DZE			10800.000	BEAD IN			
1	RPRYS	0.00001	DE			21600.000	BEAD IN			
1	RPRYC	0.00001	DE			32400.000	BEAD IN			
5	RR	0.00001	DE			43200.000	BEAD IN			
5	RCD	0.11000	DZ			54000.000	BEAD IN			
8	RCD		JRSDR			64800.000	BEAD IN			
5	RDD		JRSDR					0.000	BEAD IN	
3	RDR	0	RSUR			10800.000	BEAD IN			
5	RDR	0	RSUR			21600.000	BEAD IN			
3	RFD	200	RDIPP			32400.000	BEAD IN			
5	RFD	200	RDRTR			43200.000	BEAD IN			
3	RSD	0.50000	RSPAC			54000.000	BEAD IN			
5	RSD	0.00000	RSUR					0.000	BEAD IN	
13	RSD	0.40000	RSPAC			10800.000	BEAD IN			
14	RSD	2.00000	RSPAC			21600.000	BEAD IN			
1	RSD	2.00000	RSPAC			32400.000	BEAD IN			
1	RSD	50.00000	RSTRT			43200.000	BEAD IN			
12	RSD	10.00100	DRINARY			54000.000	BEAD IN			
3	RSD	0.00000	DVELKY					64800.000	BEAD IN	
5	RCDR		RPTSDR							
5	RCLD		RPTSDR							
5	RSD		RPRYS							
5	RSD		RPRYC							
5	RSD		RPRYP							
500	RREZ		RPRD							
200	RTCLES		RPRY							
200	RORCL		RPRC							
1.00000	RNSPAR		RPRP							
10	RATSPL									
100.00000	CRNR									
8	RSPFL									
1	RSPPR									
1	RSPPP									
1	RSP									
3	RUBS									
10	RDCR									
11	RDPY									
10	RDL									
15	RDRS									
8	RNDP									
9	RDLY									
0	RSDR									

RATHERMETRY INPUT DATA 21.0' ROADS AFTER THE BEGINNING OF THE SPILL

THE RATHERMETRY GRID HAS 18 DIVISIONS IN X SPACED 0.0157 DEGREES APART
AND 18 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.

THE (1,1) GRID LOCATION OF THE RATHERMETRY COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.35000 DEGREES LATITUDE

DEPTH VALUES IN UNITS OF METERS

DEPTH	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
13	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
12	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
11	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
10	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
9	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
8	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
7	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
6	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
5	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
4	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
3	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
2	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000
1	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000	1.000

Figure VIII.-8. Output from Main Simulation

THE COMP CELL GRID HAS 14 DIVISIONS IN X SPACED 0.0157 DEGREES APART
 AND 14 DIVISIONS IN Y SPACED 0.0157 DEGREES APART.
 THE (1,1) GRID LOCATION OF THE COMP CELL COORDINATE SYSTEM IS AT 67.00000 DEGREES LONGITUDE AND 41.35000 DEGREES LATITUDE

VALUES IN UNITS OF

Y	X ELEMENTS													
ELEMENTS	1	2	3	4	5	6	7	8	9	10	11	12	13	14
14	2	2	2	2	2	2	2	2	2	2	2	2	2	2
13	2	101	101	101	101	101	101	101	101	101	101	101	101	2
12	2	101	1	1	1	1	1	1	1	1	1	1	1	101
11	2	101	1	1	1	1	1	1	1	1	1	1	1	101
10	2	101	1	1	1	1	1	1	1	1	1	1	1	101
9	2	101	1	1	1	1	1	1	1	1	1	1	1	101
8	2	101	1	1	1	1	1	1	1	1	1	1	1	101
7	2	101	1	1	1	1	1	1	1	1	1	1	1	101
6	2	101	1	1	1	1	1	1	1	1	1	1	1	101
5	2	101	1	1	1	1	1	1	1	1	1	1	1	101
4	2	101	1	1	1	1	1	1	1	1	1	1	1	101
3	2	101	1	1	1	1	1	1	1	1	1	1	1	101
2	2	101	101	101	101	101	101	101	101	101	101	101	101	2
1	2	2	2	2	2	2	2	2	2	2	2	2	2	2

AT STEP 1 OLD SPILLER INFORMATION READ IN
 AT STEP 2 OLD SPILLER INFORMATION READ IN
 AT STEP 3 OLD CLEANUP INFORMATION READ IN

SPILL CONTROL PARAMETERS 21.000 HOURS AFTER THE BEGINNING OF THE SPILL

ENVIRONMENTAL DATA READ THIS STEP: NONE
 ADDITION OF SPILLERS OR SPILL CONTROL EFFORTS THIS STEP: 0 SPILLERS; 0 CLEANUP EFFORTS; 1 TREATMENT EFFORTS.

CHEMICAL TREATMENT EFFORTS IN PROGRESS 21.00000 HOURS AFTER THE BEGINNING OF THE SPILL

SEE TREATMENT EFFORTS BEGIN THIS STEP
 THE 1 CHEMICAL TREATMENT EFFORT IS CENTERED AT LONGITUDE 66.751900 AND LATITUDE 41.610900
 1000.000 LITERS OF DISPENSANT PER HOUR ARE USED ON AN AREA OF 1000.000 SQUARE METERS WITH AN EFFICIENCY OF 0.25 %
 THE RADIUS OVER WHICH SPILLERS TO BE TREATED ARE SEARCHED IS 10000.000 METERS
 THIS TREATMENT EFFORT STARTS 21.000000 HOURS AFTER THE BEGINNING OF THE SPILL AND LASTS 1.000000 HOURS.
 THIS TREATMENT EFFORT LOWERS THE INTERFACIAL TENSION TO 60.000000

EXISTING SPILLERS 21.000 HOURS AFTER THE BEGINNING OF THE SPILL

SPILLERS CREATED PRIOR TO THIS STEP

THE 1 SPILLER APPEARED 0.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.74850 AND LATITUDE 41.612710,
 IS OF RADIUS 2212.42 METERS AND IS OF WEIGHT 6701.2460 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.012299 GRAMS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.009988
PARAFFIN (C13-C22)	0.099975
CYCLOPARAFFIN (C6-C12)	0.001462
CYCLOPARAFFIN (C13-C22)	0.049994
AROMATIC (C6-C11)	0.000045
AROMATIC (C12-C18)	0.079955
NAPHTHENO-AROMATIC (C9-C25)	0.209957
RESIDUAL	0.100000

THE 2 SPILLER APPEARED 3.00 HOURS AFTER THE BEGINNING OF THE SPILL
 IT IS CENTERED AT LONGITUDE 66.751700 AND LATITUDE 41.611670,
 IS OF RADIUS 2042.14 METERS AND IS OF WEIGHT 6837.9600 METRIC TONS.
 SOME PROPERTIES OF THE SPILLED OIL ARE:
 DENSITY 1.009588 GRAMS/CC
 INTERFACIAL TENSION 30.000000 DYNES/CM
 KINEMATIC VISCOSITY 1.000000 CENTISTOKES

BY WEIGHT THE OIL FRACTIONS ARE:

PARAFFIN (C6-C12)	0.002130
PARAFFIN (C13-C22)	0.099988
CYCLOPARAFFIN (C6-C12)	0.007846
CYCLOPARAFFIN (C13-C22)	0.049994
AROMATIC (C6-C11)	0.000741
AROMATIC (C12-C18)	0.079908
NAPHTHENO-AROMATIC (C9-C25)	0.209955
RESIDUAL	0.100000

Figure VIII.-8. Output from Main Simulation Restarted Run

ALL HORIZONTAL VELOCITIES ARE MULTIPLIED BY 10000

U VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	1
0.26	0.28	0.31	0.31	0.36				
0.1	-0.117	-0.061	0.031	0.035	-0.008			
0.2	-0.261	-0.011	-0.036	-0.041	-0.025			
0.3	0.178	0.221	0.218	0.267	0.103			
0.4	0.285	0.329	0.132	0.160	0.178			
0.8	0.216	0.329	0.180	0.375	0.313			

U VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	2
0.26	0.28	0.31	0.31	0.36				
0.1	-0.117	-0.061	0.031	0.035	-0.008			
0.2	-0.261	-0.011	-0.036	-0.041	-0.025			
0.3	0.178	0.221	0.218	0.267	0.103			
0.4	0.285	0.329	0.132	0.160	0.178			
0.8	0.216	0.329	0.180	0.375	0.313			

U VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	3
0.26	0.28	0.31	0.31	0.36				
0.1	-0.117	-0.061	0.031	0.035	-0.008			
0.2	-0.261	-0.011	-0.036	-0.041	-0.025			
0.3	0.178	0.221	0.218	0.267	0.103			
0.4	0.285	0.329	0.132	0.160	0.178			
0.8	0.216	0.329	0.180	0.375	0.313			

V VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	1
0.26	0.28	0.31	0.31	0.36				
0.1	-0.282	-0.284	-0.267	-0.258	-0.258			
0.2	-0.471	-0.506	-0.553	-0.468	-0.438			
0.3	-0.118	-0.281	-0.219	-0.251	-0.288			
0.4	-0.186	-0.317	-0.153	-0.215	-0.172			
0.8	-0.150	-0.401	-0.406	-0.227	-0.130			

V VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	2
0.26	0.28	0.31	0.31	0.36				
0.1	-0.282	-0.284	-0.267	-0.258	-0.258			
0.2	-0.471	-0.506	-0.553	-0.468	-0.438			
0.3	-0.118	-0.281	-0.219	-0.251	-0.288			
0.4	-0.186	-0.317	-0.153	-0.215	-0.172			
0.8	-0.150	-0.401	-0.406	-0.227	-0.130			

V VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	3
0.26	0.28	0.31	0.31	0.36				
0.1	-0.282	-0.284	-0.267	-0.258	-0.258			
0.2	-0.471	-0.506	-0.553	-0.468	-0.438			
0.3	-0.118	-0.281	-0.219	-0.251	-0.288			
0.4	-0.186	-0.317	-0.153	-0.215	-0.172			
0.8	-0.150	-0.401	-0.406	-0.227	-0.130			

W VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	1
0.26	0.28	0.31	0.31	0.36				
0.1	0.000	0.000	0.000	0.000	0.000			
0.2	0.000	0.000	0.000	0.000	0.000			
0.3	0.000	0.000	0.000	0.000	0.000			
0.4	0.000	0.000	0.000	0.000	0.000			
0.8	0.000	0.000	0.000	0.000	0.000			

W VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	2
0.26	0.28	0.31	0.31	0.36				
0.1	0.000	0.000	0.000	0.000	0.000			
0.2	0.000	0.000	0.000	0.000	0.000			
0.3	0.000	0.000	0.000	0.000	0.000			
0.4	0.000	0.000	0.000	0.000	0.000			
0.8	0.000	0.000	0.000	0.000	0.000			

	0.26	0.28	0.31	0.31	0.36
0.1	0.000	0.000	0.000	0.000	0.000
0.2	0.000	0.000	0.000	0.000	0.000
0.3	0.000	0.000	0.000	0.000	0.000
0.4	0.000	0.000	0.000	0.000	0.000

W VELOCITY FIELD		STEP NUMBER		7	TIME	75600.00	LEVEL	3
0.26	0.28	0.31	0.31	0.36				
0.1	0.000	0.000	0.000	0.000	0.000			
0.2	0.000	0.000	0.000	0.000	0.000			
0.3	0.000	0.000	0.000	0.000	0.000			
0.4	0.000	0.000	0.000	0.000	0.000			

FLOATING GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1195, 0.2446) IN DEGREES WITH RESPECT TO THE FIXED DEPTH GRID
 THE BRN GRID SEPARATION IN THE FLOATING SYSTEM IS 0.0549006 DEGREES IN X AND 0.0236763 DEGREES IN Y
 THE GRID SEPARATION IN THE FIXED SYSTEM IS 0.016 DEGREES IN X AND 0.016 DEGREES IN Y

THE AVERAGE VALUES OF X, Y AND Z ARE 0.106485 0.071609 0.752923
 THE STANDARD DEVIATIONS ARE 0.028053 0.012960 0.182052

CONCENTRATION IN MG OF OIL PER ML OF WATER

	0.26	0.28	0.31	0.31	0.36
0.15	0.00000	0.00000	0.00000	0.00000	0.00000
0.20	0.00000	0.00000	0.00018	0.00052	0.00000
0.26	0.00000	0.00007	0.00017	0.00078	0.00000
0.31	0.00000	0.00002	0.00008	0.00001	0.00000
0.36	0.00000	0.00000	0.00000	0.00000	0.00000

CONCENTRATION IN MG OF OIL PER ML OF WATER

	0.26	0.28	0.31	0.31	0.36
0.15	0.00000	0.00000	0.00000	0.00000	0.00000
0.20	0.00000	0.00007	0.00008	0.00197	0.00000
0.26	0.00000	0.00017	0.00078	0.00099	0.00000
0.31	0.00000	0.00000	0.00016	0.00007	0.00000
0.36	0.00000	0.00000	0.00000	0.00000	0.00000

CONCENTRATION IN MG OF OIL PER ML OF WATER

	0.26	0.28	0.31	0.31	0.36
0.15	0.00000	0.00000	0.00000	0.00000	0.00000
0.20	0.00000	0.00101	0.00088	0.01098	0.00000
0.26	0.00000	0.00001	0.00157	0.00409	0.00000
0.31	0.00000	0.00017	0.00086	0.00017	0.00000
0.36	0.00000	0.00000	0.00000	0.00000	0.00000

Figure VIII.-8. Output from Main Simulation Restarted Run

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IN DEGREES & IN METERS
 PARTICLE PARAMETERS AT TIME 75000.00

#	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION FIELD SYSTEM			PARTICLE PARAMETERS			
	X	Y	Z	X	Y	Z	DIAPHRAGM	DENSITY	SGT. VEL.	BISS
1	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
2	0.0911	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
3	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
4	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
5	0.0911	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
6	0.0911	0.0819	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
7	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
8	0.0912	0.0820	0.1022	0.211	0.327	0.1022	0.0010	0.8770	0.0000	0.998
9	0.0918	0.0820	0.8150	0.211	0.327	0.8150	0.0010	0.8770	0.0000	0.998
10	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
11	0.0913	0.0819	0.1865	0.211	0.327	0.1865	0.0010	0.8770	0.0000	0.998
12	0.0912	0.0819	0.5872	0.213	0.327	0.5872	0.0010	0.8770	0.0000	0.998
13	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
14	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
15	0.0912	0.0821	0.1558	0.211	0.327	0.1558	0.0010	0.8770	0.0000	0.998
16	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
17	0.0912	0.0820	0.8167	0.213	0.327	0.8167	0.0010	0.8770	0.0000	0.998
18	0.0911	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
19	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
20	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
21	0.0911	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
22	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
23	0.0912	0.0821	0.1918	0.213	0.327	0.1918	0.0010	0.8770	0.0000	0.998
24	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
25	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
26	0.0912	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
27	0.0911	0.0821	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
28	0.0912	0.0822	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
29	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
30	0.0911	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
31	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
32	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
33	0.0911	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
34	0.0911	0.0820	0.1608	0.213	0.327	0.1608	0.0010	0.8770	0.0000	0.998
35	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
36	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
37	0.0913	0.0821	0.5818	0.213	0.327	0.5818	0.0010	0.8770	0.0000	0.998
38	0.0912	0.0820	0.8150	0.213	0.327	0.8150	0.0010	0.8770	0.0000	0.998
39	0.0913	0.0820	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
40	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
41	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
42	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
43	0.0920	0.0822	0.8150	0.215	0.297	0.8150	0.0010	1.0012	0.0000	1.001
44	0.0917	0.0831	0.8150	0.211	0.327	0.8150	0.0010	1.0012	0.0000	1.001
45	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
46	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	1.0012	0.0000	1.001
47	0.0920	0.0828	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
48	0.0925	0.0829	0.8150	0.212	0.327	0.8150	0.0010	0.8770	0.0000	0.998
49	0.0920	0.0819	0.8150	0.202	0.296	0.8150	0.0010	1.0012	0.0000	1.001
50	0.0900	0.0890	0.8150	0.209	0.178	0.8150	0.0010	1.0012	0.0000	1.001

Figure VIII.-8. Output from Main Simulation
 Restarted Run

53	0.0750	0.0711	0.8150	0.218	0.118	0.8150	0.0010	1.0012	0.0000	1.001
52	0.0754	0.0611	0.8150	0.215	0.106	0.8150	0.0010	1.0012	0.0000	1.001
51	0.0718	0.0670	0.8150	0.217	0.107	0.8150	0.0010	1.0012	0.0000	1.001
50	0.0956	0.0611	0.8150	0.215	0.106	0.8150	0.0010	1.0012	0.0000	1.001
55	0.0978	0.0878	0.8150	0.212	0.177	0.8150	0.0010	0.8770	0.0000	0.998
56	0.0978	0.0877	0.8150	0.212	0.177	0.8150	0.0010	0.8770	0.0000	0.998
57	0.0911	0.0671	0.8150	0.211	0.112	0.8150	0.0010	1.0012	0.0000	1.001
58	0.0921	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
59	0.1182	0.0715	0.8150	0.258	0.118	0.8150	0.0010	1.0012	0.0000	1.001
60	0.0965	0.0609	0.8150	0.216	0.105	0.8150	0.0010	1.0012	0.0000	1.001
61	0.0910	0.0583	0.8150	0.202	0.103	0.8150	0.0010	1.0012	0.0000	1.001
62	0.0928	0.0628	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
63	0.0919	0.0572	0.8150	0.211	0.102	0.8150	0.0010	1.0012	0.0000	1.001
64	0.1150	0.0688	0.8150	0.230	0.109	0.8150	0.0010	1.0012	0.0000	1.001
65	0.0950	0.0602	0.8150	0.215	0.105	0.8150	0.0010	1.0012	0.0000	1.001
66	0.0978	0.0585	0.8150	0.217	0.103	0.8150	0.0010	1.0012	0.0000	1.001
67	0.0928	0.0827	0.8786	0.212	0.127	0.8786	0.0010	0.8770	0.0000	0.998
68	0.0988	0.0618	0.8150	0.218	0.105	0.7611	0.0010	1.0012	0.0000	1.001
69	0.0969	0.0610	0.8150	0.216	0.108	0.8150	0.0010	1.0012	0.0000	1.001
70	0.0949	0.0578	0.8150	0.218	0.102	0.8150	0.0010	1.0012	0.0000	1.001
71	0.0979	0.0627	0.8150	0.217	0.107	0.8150	0.0010	1.0012	0.0000	1.001
72	0.0921	0.0829	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
73	0.0923	0.0828	0.8150	0.212	0.127	0.7678	0.0010	0.8770	0.0000	0.998
74	0.0978	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
75	0.0920	0.0828	0.8150	0.212	0.127	0.7887	0.0010	0.8770	0.0000	0.998
76	0.0920	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
77	0.0923	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
78	0.0928	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
79	0.0923	0.0827	0.8150	0.212	0.127	0.7275	0.0010	0.8770	0.0000	0.998
80	0.0923	0.0827	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
81	0.0928	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
82	0.0928	0.0828	0.8150	0.212	0.127	0.8150	0.0010	0.8770	0.0000	0.998
83	0.0928	0.0828	0.7111	0.212	0.127	0.7111	0.0010	0.8770	0.0000	0.998
84	0.0928	0.0827	0.8150	0.218	0.108	0.8150	0.0010	0.9952	0.0000	0.998
85	0.0986	0.0755	0.8150	0.218	0.280	0.8150	0.0010	1.0095	0.0000	1.069
86	0.0995	0.0865	0.8150	0.219	0.291	0.8150	0.0010	1.0095	0.0000	1.069
87	0.0971	0.0861	0.8150	0.217	0.291	0.8150	0.0010	1.0095	0.0000	1.069
88	0.0918	0.0807	0.7189	0.211	0.285	0.7189	0.0010	1.0095	0.0000	1.069
89	0.1058	0.0879	0.8150	0.225	0.312	0.8150	0.0010	0.9952	0.0000	0.998
90	0.0981	0.0818	0.8150	0.218	0.281	0.8150	0.0010	1.0095	0.0000	1.069
91	0.0919	0.0810	0.8150	0.211	0.108	0.8150	0.0010	0.9952	0.0000	0.998
92	0.0951	0.0661	0.7013	0.215	0.311	0.2013	0.0010	0.9952	0.0000	0.998
93	0.0942	0.0702	0.8150	0.218	0.315	0.8150	0.0010	0.9952	0.0000	0.998
94	0.1193	0.0718	0.8150	0.219	0.316	0.8150	0.0010	0.9952	0.0000	0.998
95	0.0958	0.0505	0.8150	0.215	0.295	0.8150	0.0010	1.0105	0.0000	0.999
96	0.1128	0.0703	0.8150	0.213	0.315	0.315	0.0010	1.0002	0.0000	0.981
97	0.1116	0.0577	0.8150	0.251	0.102	0.8150	0.0010	1.0105	0.0000	0.999
98	0.1255	0.0892	0.8150	0.285	0.298	0.8150	0.0010	1.0105	0.0000	0.999
99	0.1118	0.0651	0.5017	0.211	0.118	0.5017	0.0010	1.0002	0.0000	0.981
100	0.1090	0.0706	0.8150	0.219	0.315	0.8150	0.0010	1.0002	0.0000	0.981
101	0.1188	0.0681	0.8150	0.213	0.318	0.8150	0.0010	1.0002	0.0000	0.981
102	0.1127	0.0689	0.5087	0.212	0.118	0.5087	0.0010	1.0002	0.0000	0.981
103	0.1452	0.0886	0.8150	0.265	0.311	0.8150	0.0010	1.0018	0.0000	0.993
104	0.1438	0.0887	0.8150	0.261	0.325	0.8150	0.0010	1.0018	0.0000	0.993
105	0.1295	0.0527	0.6953	0.289	0.297	0.6953	0.0010	1.0112	0.0000	1.086
106	0.1378	0.0686	0.8150	0.257	0.309	0.8150	0.0010	1.0112	0.0000	1.086
107	0.1080	0.0618	0.8150	0.228	0.308	0.8150	0.0010	1.0018	0.0000	0.993
108	0.1825	0.0780	0.8150	0.262	0.321	0.8150	0.0010	1.0018	0.0000	0.993
109	0.1825	0.0686	0.8150	0.272	0.309	0.8150	0.0010	1.0068	0.0000	1.030
110	0.1885	0.0718	0.8188	0.268	0.318	0.8188	0.0010	1.0068	0.0000	1.030
111	0.1888	0.0837	0.8150	0.258	0.288	0.8150	0.0010	1.0117	0.0000	0.998
112	0.1858	0.0888	0.8150	0.275	0.289	0.8150	0.0010	1.0117	0.0000	0.998
113	0.1816	0.0723	0.8150	0.261	0.317	0.8150	0.0010	1.0068	0.0000	1.030
114	0.1215	0.0519	0.8150	0.293	0.297	0.8150	0.0010	1.0117	0.0000	0.998
115	0.1118	0.0669	0.8150	0.253	0.312	0.8150	0.0010	1.0068	0.0000	1.030
116	0.1718	0.0820	0.8150	0.291	0.287	0.8150	0.0010	1.0120	0.0000	1.055
117	0.1761	0.0878	0.5988	0.296	0.292	0.5988	0.0010	1.0120	0.0000	1.055
118	0.1588	0.0515	0.1826	0.279	0.296	0.1826	0.0010	1.0120	0.0000	1.055
119	0.1587	0.0708	0.8150	0.278	0.315	0.8150	0.0010	1.0081	0.0000	0.959
120	0.1522	0.0727	0.5980	0.272	0.317	0.5980	0.0010	1.0083	0.0000	0.959
121	0.1318	0.0776	0.8150	0.253	0.322	0.8150	0.0010	1.0083	0.0000	0.959
122	0.1668	0.0711	0.8150	0.286	0.316	0.8150	0.0010	1.0096	0.0000	1.078
123	0.1517	0.0515	0.8150	0.271	0.296	0.8150	0.0010	1.0123	0.0000	0.988
124	0.1886	0.0722	0.8150	0.268	0.317	0.8150	0.0010	1.0096	0.0000	1.078
125	0.1922	0.0889	0.8150	0.312	0.298	0.8150	0.0010	1.0123	0.0000	0.988
126	0.1671	0.0715	0.8150	0.287	0.316	0.8150	0.0010	1.0096	0.0000	1.078
127	0.1671	0.0716	0.8150	0.287	0.316	0.8150	0.0010	1.0096	0.0000	1.078

BASE BALANCE

TOTAL MASS OF OIL SPILLED 20000.00000 METRIC TONS

LOCATION OF OIL	AMOUNT (METRIC TONS)	PERCENT OF TOTAL
IN ATMOSPHERE	5080.60100	25.40
ON SURFACE	11898.18000	59.49
IN WATER COLUMN	110.18400	0.55
ON BEACH	98.98161	0.47
ON SHIP	0.00000	0.00
REMOVAL MECHANISMS		
BIOLOGICALLY DEGRADED	0.00000	0.00
PHYSICALLY CLEAVED UP	1200.00000	6.00
LOST THRU OPPER MOUNTAIN	0.00000	0.00
LOST PARTICLES		

Figure VIII.-8. Output from Main Simulation
Restarted Run


```

INPUT PARAMETERS
  IN      RST
  1      RPL17
          MASS IN METRIC TONS

      YEAR  ATROSSPREP  RIO CONCEN  DEPOSITEN  CLIPSED DP  HORPPD  LOST  1R 4000?  1R SURFACE  1R WATER
0.0      2271.017      0.0          29.011      0.0        10000.000  0.0    3.2      3660.902      18.088
3.000    4419.047      0.0          41.947      0.0        20000.000  0.0    3.2     15115.957     82.994
6.000    6678.738      0.0          66.946      0.0        20000.000  0.0    3.0     15160.184     84.047
9.000    8936.273      0.0          71.923      0.0        20000.000  0.0    3.0     16997.855     111.967
12.000   1117.305      0.0          81.085     600.000    20000.000  0.0    3.2     16271.519     100.011
15.000   5001.203      0.0          85.858    1200.000    20000.000  0.0    3.0     17595.823     116.968
18.000   5088.727      0.0          90.944    1200.000    20000.000  0.0    3.0     17539.262     121.008
21.000   5080.602      0.0          91.091    1200.000    20000.000  0.0    3.2     17598.189     117.082
24.000   5103.215      0.0          96.956    1200.000    20000.000  0.0    3.2     17661.906     117.816
27.000   5119.657      0.0         101.009    1200.000    20000.000  0.0    3.2     17616.502     982.811

FOR PLOT HORPPD  1
MASS IN WATER COLUMN PLOTTED
MASS PHYSICALLY CLEARED BY PLOTTED
MASS ON THE SURFACE PLOTTED
MASS IN ATMOSPHERE PLOTTED

```

Figure VIII.-9. Output from Program PLOTMASS

MASS DISTRIBUTION

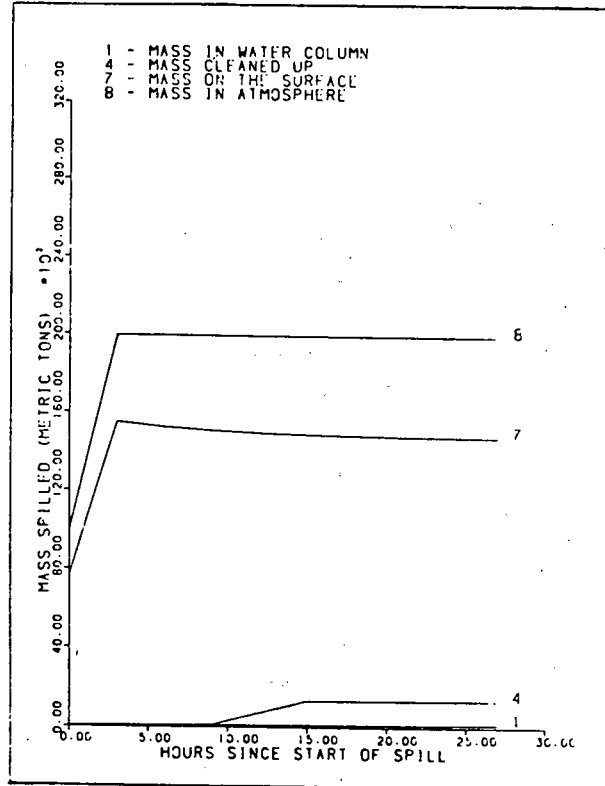


Figure VIII.-10. Plot from Program PLOTMASS

```

INPUT PARAMETERS
1  SPAT
1  ISCAL
1  MROCP
10 MROCP
0  MROPT
0.05000 CCUT

```

JULIAN DATE	HOURS	SICR	SPILL	POP	SPILLETS	REN	LONG	MAX LOG	MIN LAT	MAX LAT	BLERBETS	BBBLE			
0.0	1														
1	0.0	66.820	41.670	25.000	10000.000	0.877	10.000	1.000							
	0.05	0.10	0.11	0.05	0.10	0.08	0.21	0.30							
5	5	3 30	1 10	0 0 20											
	0.0	6.055	9.935	0.0	0.000	0.000	0.330	67.000000	41.349991	0.0		0.035700	0.035700		
0.215	0.216	0.216	0.216	0.216											
0.356	0.356	0.356	0.356	0.356											
0.0	0.0	0.0	0.0	0.0	0.0	0.0	4.61	18.25	3.05	0.0	0.0	6.13	36.41	0.27	0.0
0.0	0.66	5.25	0.01	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.06	42.94	7.07	0.00	0.0	17.52	84.28	5.81	0.00
0.0	2.38	20.60	2.82	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0	29.98	63.81	32.88	0.01	0.0	187.49	439.60	51.40	0.02
0.0	46.89	120.17	7.14	0.0	0.0	0.0	0.0	0.04	0.00	0.0					
3.0	2														
1	0.0	66.817	41.650	1093.988	7660.906	1.003	10.000	1.000							
	0.01	0.10	0.02	0.05	0.00	0.08	0.21	0.30							
2	3.000	66.820	41.670	25.800	10000.000	0.877	10.000	1.000							
	0.05	0.10	0.11	0.05	0.10	0.08	0.21	0.30							
5	5	3 83	2 10	1 0 62											
	10800.000	5.118	8.494	0.0	0.017	0.015	0.330	67.000000	41.349991	0.0		0.035700	0.035700		
0.189	0.205	0.221	0.238	0.254											
0.311	0.326	0.341	0.356	0.371											
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0
0.0	0.00	0.01	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.00
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00	0.01	0.00	0.00	0.0	0.0	0.01	0.01	0.00
0.0	0.02	0.08	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.00	0.00
6.0	2														
1	0.0	66.811	41.632	1300.711	7817.359	1.009	10.000	1.000							
	0.00	0.10	0.01	0.05	0.00	0.08	0.21	0.30							
2	3.000	66.815	41.633	1094.729	7999.602	0.995	10.000	1.000							
	0.01	0.10	0.08	0.05	0.01	0.08	0.21	0.30							
5	5	3 84	2 10	2 0 67											
	21600.000	4.999	7.494	0.0	0.019	0.024	0.330	67.000000	41.349991	0.0		0.035700	0.035700		
0.191	0.209	0.226	0.244	0.261											
0.288	0.308	0.322	0.336	0.379											
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.00	0.00	0.00
0.0	0.00	0.00	0.00	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.00	0.01	0.00
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.00	0.00	0.00
0.0	0.02	0.02	0.00	0.0	0.0	0.0	0.00	0.00	0.00	0.00	0.0	0.0	0.00	0.00	0.00
9.0	2														
1	0.0	66.800	41.627	1446.972	7378.888	1.110	10.000	1.000							
	0.00	0.10	0.01	0.05	0.00	0.08	0.21	0.30							
2	3.000	66.803	41.604	1101.411	7791.707	1.100	10.000	1.000							

Figure VIII.-11. Input to Program DATAOUT from Main Program

```

0.01 0.10 0.01 0.05 0.01 0.08 0.21 0.10
5 5 3 102 8 10 3 0 78
32400.000 4.874 7.161 0.0 0.021 0.024 0.110 67.000000 41.149991 0.0 0.035700 0.035700
0.188 0.207 0.226 0.246 0.265
0.275 0.300 0.326 0.351 0.377
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.01 0.01 0.00 0.00
12.0 2
1 0.0 66.787 41.624 1688.980 7349.875 1.011 10.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.791 41.644 1497.641 7637.984 1.008 10.000 1.000
0.01 0.10 0.02 0.05 0.00 0.08 0.21 0.30
5 5 3 108 8 10 4 0 81
43200.000 4.565 7.211 0.0 0.027 0.024 0.130 67.000000 41.349991 0.0 0.035700 0.035700
0.179 0.205 0.232 0.258 0.284
0.275 0.299 0.323 0.347 0.371
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.0 0.0 0.01 0.01 0.00 0.00
0.0 0.02 0.01 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.0 0.0
15.0 2
1 0.0 66.778 41.620 1866.227 7029.102 1.012 10.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.778 41.641 1685.621 7244.434 1.006 10.000 1.000
0.00 0.10 0.01 0.05 0.00 0.08 0.21 0.30
5 5 3 115 10 10 5 0 86
54000.000 4.247 7.109 0.0 0.034 0.024 0.130 67.000000 41.349991 0.0 0.035700 0.035700
0.172 0.204 0.236 0.269 0.301
0.270 0.294 0.318 0.342 0.366
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.01 0.01 0.00 0.00
0.0 0.01 0.01 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
18.0 2
1 0.0 66.762 41.617 2041.777 6713.637 1.012 10.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.765 41.617 1866.847 6842.160 1.008 10.000 1.000
0.00 0.10 0.01 0.05 0.00 0.08 0.21 0.30
5 5 3 121 12 10 6 0 91

```

Figure VIII.-11. Input to Program DATAOUT from Main Program

```

64800.000 3.743 6.982 0.0 0.046 0.024 0.330 67.000000 41.349991 0.0 0.035700 0.035700
0.159 0.303 0.246 0.290 0.334
0.266 0.290 0.313 0.337 0.361
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.01 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
21.0 2
1 0.0 66.748 41.613 2212.425 6701.297 1.012 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.752 41.634 2082.376 6837.961 1.010 30.000 1.000
0.00 0.10 0.01 0.05 0.00 0.08 0.21 0.30
5 5 3 129 14 10 7 0 93
75600.000 3.448 6.806 0.0 0.052 0.024 0.330 67.000000 41.349991 0.0 0.035700 0.035700
0.151 0.302 0.253 0.303 0.354
0.258 0.283 0.308 0.332 0.357
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.01 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
24.0 2
1 0.0 66.734 41.609 2378.807 6689.898 1.012 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.737 41.631 2213.033 6806.285 1.011 30.000 1.000
0.00 0.10 0.01 0.05 0.00 0.08 0.21 0.30
5 5 3 135 16 10 8 0 97
86400.000 3.223 6.720 0.0 0.058 0.024 0.330 67.000000 41.349991 0.0 0.035700 0.035700
0.146 0.302 0.258 0.314 0.370
0.252 0.279 0.304 0.333 0.360
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.01 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
27.0 2
1 0.0 66.720 41.606 2541.371 6681.457 1.013 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.722 41.627 2379.377 6780.445 1.011 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
5 5 3 140 18 10 9 0 101
97200.000 2.442 6.543 0.0 0.072 0.025 0.330 67.000000 41.349991 0.0 0.035700 0.035700
0.132 0.302 0.271 0.341 0.411
0.248 0.275 0.303 0.310 0.347
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.01 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
30.0 2
1 0.0 66.705 41.602 2700.542 6674.250 1.013 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
2 3.000 66.707 41.624 2541.933 6762.348 1.012 30.000 1.000
0.00 0.10 0.00 0.05 0.00 0.08 0.21 0.30
5 5 3 145 20 10 10 0 104
108000.000 2.331 6.366 0.0 0.079 0.024 0.330 67.000000 41.349991 0.0 0.035700 0.035700
0.124 0.302 0.279 0.356 0.433
0.246 0.271 0.295 0.320 0.345
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.0 0.0 0.00 0.00 0.00 0.0
0.0 0.00 0.00 0.00 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.00 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00
0.0 0.01 0.00 0.00 0.00 0.0 0.0 0.0 0.00 0.00 0.00 0.00 0.0 0.00 0.00 0.00

```

***** POP ENCODING PD ON UNIT 1

Figure VIII.-11. Input to Program DATAOUT from Main Program

INPUT PARAMETERS
 -1 WPT
 2 ISCAL
 1 WDSR
 10 WDCR
 0 WOPT
 0.05000 CCUT

JULIAN DATE	HOOPS SINCE SPILL	#OF SPILLETS	HIP LONG	WAE LONG	HIP LAT	WAE LAT	ELEVENTS	ANGLE
350	0.0	1	66.8193	66.8190	41.6691	41.6698	13	0.0
350	3.00000	2	66.8269	66.7921	41.6400	41.6700	8	0.0
350	6.00000	2	66.8286	66.7903	41.6177	41.6655	8	0.0
350	9.00000	2	66.8103	66.7888	41.6111	41.6609	9	0.0
350	12.00000	2	66.8317	66.7771	41.6088	41.6563	9	0.0
350	15.00000	2	66.8330	66.7688	41.6038	41.6515	9	0.0
350	18.00000	2	66.8337	66.7626	41.5992	41.6467	9	0.0
350	21.00000	2	66.8140	66.7393	41.5935	41.6418	9	0.0
351	24.00000	2	66.8182	66.7188	41.5897	41.6371	9	0.0
351	27.00000	2	66.8181	66.6911	41.5888	41.6342	9	0.0
351	30.00000	2	66.8339	66.6759	41.5800	41.6313	9	0.0

***** EOF ENCOUNTERED ON UNIT 1

Figure VIII.-12. Output of Program DATAOUT

INPUT PARAMETERS
 1 UNIT
 1 HMOCK

SPILLET PARAMETERS FOR JULIAN DAY 150 WHICH IS 0.0 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.81999	61.67000	25.00000	5.80726

THE GRID SEPARATION IN THE X DIRECTION IS 9.40 METERS AND IN THE Y DIRECTION IS 9.71 METERS
 THERE ARE 13 GRIDS OVER THE RESINUM CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 W 61.350 N

LONGITUDE	LATITUDE	PARTS/BILLION
66.8193	61.6691	18209810.00
66.8191	61.6692	70586560.00
66.8191	61.6691	16502773.00
66.8192	61.6691	80311316.00
66.8192	61.6692	*****
66.8192	61.6691	88678680.00
66.8192	61.6698	11112.86
66.8191	61.6691	1831701.00
66.8191	61.6692	18895128.00
66.8191	61.6693	3321670.00
66.8191	61.6698	137.98
66.8190	61.6691	8608.81
66.8190	61.6692	6818.01

MINIMUM LONGITUDE 66.81900
 MINIMUM LONGITUDE 66.81938
 MINIMUM LATITUDE 61.66916
 MINIMUM LATITUDE 61.66910

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 3.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.81670	61.68669	1091.98808	0.00201
2	66.81999	61.67000	25.00000	5.80726

THE GRID SEPARATION IN THE X DIRECTION IS 1445.81 METERS AND IN THE Y DIRECTION IS 1666.16 METERS
 THERE ARE 8 GRIDS OVER THE RESINUM CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 W 61.150 N

LONGITUDE	LATITUDE	PARTS/BILLION
66.8269	61.6800	1067.11
66.8269	61.6550	1942.87
66.8269	61.6700	6151.87
66.8095	61.6800	2197.70
66.8095	61.6550	1788.29
66.8095	61.6700	15488.80

Figure VIII.-13. Output of Program CHECDATA

66.7921 01.6000 174.19
 66.7921 01.6550 440.24

BEGINN LONGITUDE 66.79207
 BEGINN LONGITUDE 66.82687
 BEGINN LATITUDE 01.64598
 BEGINN LATITUDE 01.69007

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 6.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.81145	01.63202	1300.71118	0.00118
2	66.81648	01.65104	1090.72925	0.00213

THE GRID SEPARATION IN THE X DIRECTION IS 1548.05 METERS AND IN THE Y DIRECTION IS 2646.45 METERS
 THERE ARE 8 GRIDS OVER THE RIVERIN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 01.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8284	01.6177	151.59
66.8284	01.6416	1706.07
66.8284	01.6655	6491.90
66.8094	01.6177	769.16
66.8094	01.6416	1557.80
66.8094	01.6655	9072.68
66.7903	01.6416	141.55
66.7903	01.6655	125.12

BEGINN LONGITUDE 66.79031
 BEGINN LONGITUDE 66.82655
 BEGINN LATITUDE 01.64553
 BEGINN LATITUDE 01.61776

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 9.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.79470	01.62717	1696.97241	0.00108
2	66.80272	01.64812	1301.81113	0.00146

THE GRID SEPARATION IN THE X DIRECTION IS 1740.98 METERS AND IN THE Y DIRECTION IS 2662.14 METERS
 THERE ARE 9 GRIDS OVER THE RIVERIN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 01.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8103	01.6111	171.76
66.8103	01.6370	1983.86
66.8103	01.6609	6729.10
66.8091	01.6111	716.51

66.8091 01.6170 1658.51
 66.8091 01.6609 7702.15
 66.7988 01.6111 175.82
 66.7988 01.6170 674.87
 66.7988 01.6609 205.42

BEGINN LONGITUDE 66.79470
 BEGINN LONGITUDE 66.81109
 BEGINN LATITUDE 01.64095
 BEGINN LATITUDE 01.61107

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 12.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.79070	01.62374	1688.98081	0.00081
2	66.79070	01.64479	1007.64111	0.00108

THE GRID SEPARATION IN THE X DIRECTION IS 2270.50 METERS AND IN THE Y DIRECTION IS 2661.08 METERS
 THERE ARE 9 GRIDS OVER THE RIVERIN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 01.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8117	01.6088	472.18
66.8117	01.6323	2081.39
66.8117	01.6563	4598.70
66.8044	01.6088	515.67
66.8044	01.6323	2721.92
66.8044	01.6563	4609.82
66.7771	01.6088	118.73
66.7771	01.6323	675.27
66.7771	01.6563	289.74

BEGINN LONGITUDE 66.77704
 BEGINN LONGITUDE 66.80173
 BEGINN LATITUDE 01.64627
 BEGINN LATITUDE 01.60821

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 15.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.77800	01.62022	1884.22774	0.00063
2	66.77800	01.64072	1684.62105	0.00081

THE GRID SEPARATION IN THE X DIRECTION IS 2811.98 METERS AND IN THE Y DIRECTION IS 2651.20 METERS
 THERE ARE 9 GRIDS OVER THE RIVERIN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 01.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8103	01.6111	171.76
66.8103	01.6370	1983.86
66.8103	01.6609	6729.10
66.8091	01.6111	716.51

Figure VIII.-13. Output of Program CHECDATA

66.8110 41.6018 474.24
 66.8110 41.6277 2017.44
 66.8110 41.6515 6021.82
 66.7989 41.6018 474.24
 66.7989 41.6277 2218.31
 66.7989 41.6515 3185.28
 66.7688 41.6018 196.88
 66.7688 41.6277 689.75
 66.7688 41.6515 269.50

BEGINN LONGITUDE 66.7688
 BEGINN LONGITUDE 66.8126
 BEGINN LATITUDE 41.6515
 BEGINN LATITUDE 41.6018

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 18.0000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.76161	41.61665	2081.77486	0.00051
2	66.76510	41.61715	1866.98741	0.00062

THE GRID SEPARATION IN THE X DIRECTION IS 3787.19 METERS AND IN THE Y DIRECTION IS 2642.64 METERS
 THERE ARE 9 GRIDS OVER THE BEGINN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 W 41.350 N

LONGITUDE LATITUDE PARTS/BILLION
 66.8137 41.5992 186.60
 66.8137 41.6230 1887.91
 66.8137 41.6467 9052.05
 66.7982 41.5992 181.06
 66.7982 41.6210 1772.21
 66.7982 41.6467 2100.01
 66.7826 41.5992 208.22
 66.7826 41.6210 305.61
 66.7826 41.6467 158.78

BEGINN LONGITUDE 66.7826
 BEGINN LONGITUDE 66.8172
 BEGINN LATITUDE 41.6467
 BEGINN LATITUDE 41.5992

SPILLET PARAMETERS FOR JULIAN DAY 350 WHICH IS 21.0000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.78886	41.61273	2232.82980	0.00041
2	66.79171	41.61362	2082.37622	0.00052

THE GRID SEPARATION IN THE X DIRECTION IS 4352.18 METERS AND IN THE Y DIRECTION IS 2487.18 METERS
 THERE ARE 9 GRIDS OVER THE BEGINN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 W 41.350 N

LONGITUDE LATITUDE PARTS/BILLION
 66.8140 41.5915 135.58
 66.8140 41.6177 1609.28
 66.8140 41.6418 4560.07
 66.7815 41.5915 126.60
 66.7815 41.6177 1512.88
 66.7815 41.6418 1811.28
 66.7291 41.5915 287.28
 66.7291 41.6177 369.77
 66.7291 41.6418 248.99

BEGINN LONGITUDE 66.7291
 BEGINN LONGITUDE 66.8185
 BEGINN LATITUDE 41.6418
 BEGINN LATITUDE 41.5918

SPILLET PARAMETERS FOR JULIAN DAY 351 WHICH IS 24.0000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.71194	41.60922	2178.80668	0.00037
2	66.71669	41.61000	2231.03296	0.00088

THE GRID SEPARATION IN THE X DIRECTION IS 4791.81 METERS AND IN THE Y DIRECTION IS 2633.03 METERS
 THERE ARE 9 GRIDS OVER THE BEGINN CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 W 41.350 N

LONGITUDE LATITUDE PARTS/BILLION
 66.8182 41.5897 155.99
 66.8182 41.6138 1706.01
 66.8182 41.6371 4246.80
 66.7765 41.5897 112.06
 66.7765 41.6138 1805.29
 66.7765 41.6371 1758.88
 66.7188 41.5897 200.75
 66.7188 41.6138 417.99
 66.7188 41.6371 171.07

BEGINN LONGITUDE 66.7188
 BEGINN LONGITUDE 66.8185
 BEGINN LATITUDE 41.61705
 BEGINN LATITUDE 41.58971

SPILLET PARAMETERS FOR JULIAN DAY 351 WHICH IS 27.0000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.71962	41.60558	2541.17061	0.00013

Figure VIII.-13. Output of Program CHECDATA

2 66.72198 81.62786 2179.17788 0.00016
 THE GRID SEPARATION IN THE X DIRECTION IS 5966.00 METERS AND IN THE Y DIRECTION IS 2742.11 METERS
 THERE ARE 9 GRIDS OVER THE MINIMUM CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 81.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8181	81.5888	122.62
66.8181	81.6095	1792.17
66.8181	81.6382	3109.69
66.7626	81.5888	276.48
66.7626	81.6095	1284.40
66.7626	81.6382	1193.10
66.6911	81.5888	125.85
66.6911	81.6095	101.23
66.6911	81.6382	187.11

MINIMUM LONGITUDE 66.69106
 MINIMUM LONGITUDE 66.81811
 MINIMUM LATITUDE 81.63817
 MINIMUM LATITUDE 81.58888

SPILLET PARAMETERS FOR JULIAN DAY 151 WHICH IS 10.00000 HOURS FROM THE START OF THE SPILL

SPILLET LOCATIONS AND RADII

SPILLET #	LONGITUDE	LATITUDE	RADIUS	THICKNESS
1	66.70529	81.60596	2700.58288	0.00029
2	66.70706	81.62811	2581.91111	0.00013

THE GRID SEPARATION IN THE X DIRECTION IS 6570.71 METERS AND IN THE Y DIRECTION IS 2850.95 METERS
 THERE ARE 9 GRIDS OVER THE MINIMUM CONCENTRATION

THE DEPTH GRID HAS BEEN ROTATED 0.0 IN THE COUNTER CLOCKWISE DIRECTION
 AND HAS AN ORIGIN AT 67.000 N 81.350 W

LONGITUDE	LATITUDE	PARTS/BILLION
66.8119	81.5800	112.04
66.8119	81.6056	1881.85
66.8119	81.6313	2852.70
66.7589	81.5800	286.10
66.7589	81.6056	1192.99
66.7589	81.6313	1098.89
66.6759	81.5800	187.00
66.6759	81.6056	182.78
66.6759	81.6313	167.20

MINIMUM LONGITUDE 66.67587
 MINIMUM LONGITUDE 66.81196
 MINIMUM LATITUDE 81.63127
 MINIMUM LATITUDE 81.57999

***** EOF ENCOUNTERED ON UNIT 1

THIS RUN STARTED ON DAY 351800 IT IS 27.000000 AFTER THE START OF THE SPILL

***** CASE 1 *****

LONGITUDE	LATITUDE	RADIUS	THICKNESS
66.720	61.605	2309.373	0.000375
66.722	61.627	2370.377	0.000377

TABLE 100 9 CONCENTRATION VALUES OUT THREE.

LONGITUDE	LATITUDE	PARTS/BILLION
66.830	61.585	322.667
66.830	61.610	1792.372
66.830	61.630	3109.690
66.763	61.585	776.485
66.763	61.610	1246.393
66.763	61.630	1297.300
66.691	61.585	125.053
66.691	61.610	301.231
66.691	61.630	167.109

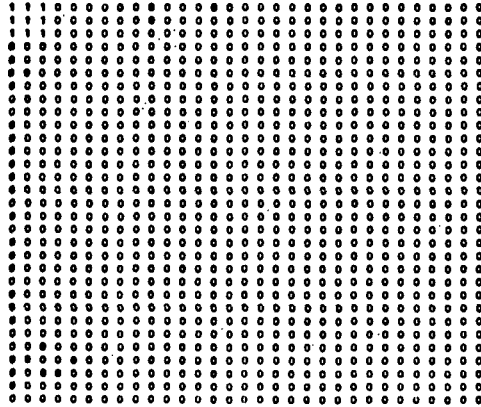


Figure VIII.-14. Output of Program PLOTMAP

15.0 HOURS AFTER START OF THE SPILL
MAP OF SPILLETS AND SUBSURFACE

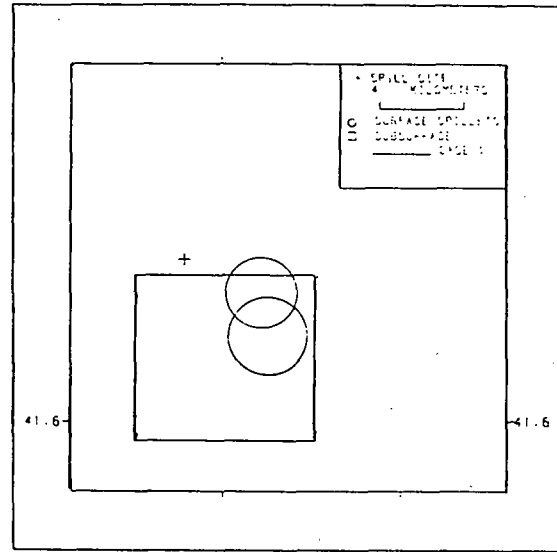


Figure VIII.-15. Plot from PLOTMAP

```

INPUT  PARAMETERS
      1      WAB
      1      SPLOT
      0.0    THICK
      10     NSTRP

```

NON PLOTTING CASE

THERE ARE	13 CONCENTRATION VALUES AND 1 SPILLETTS OUT THERE AT TIME	0.0 HOURS
	0.0020 SQUARE KILOMETERS ON SURFACE	
	0.0012 SQUARE KILOMETERS IN SUBSURFACE	
	0.0032 TOTAL AREA EXTENT	
THERE ARE	8 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	3.00 HOURS
	3.7616 SQUARE KILOMETERS ON SURFACE	
	19.2723 SQUARE KILOMETERS IN SUBSURFACE	
	23.0341 TOTAL AREA EXTENT	
THERE ARE	8 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	6.00 HOURS
	9.0801 SQUARE KILOMETERS ON SURFACE	
	33.7698 SQUARE KILOMETERS IN SUBSURFACE	
	42.8499 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	9.00 HOURS
	12.3609 SQUARE KILOMETERS ON SURFACE	
	41.7117 SQUARE KILOMETERS IN SUBSURFACE	
	54.0726 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	12.00 HOURS
	15.9458 SQUARE KILOMETERS ON SURFACE	
	54.3769 SQUARE KILOMETERS IN SUBSURFACE	
	70.3227 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	15.00 HOURS
	19.8678 SQUARE KILOMETERS ON SURFACE	
	67.5601 SQUARE KILOMETERS IN SUBSURFACE	
	87.4281 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	18.00 HOURS
	24.0456 SQUARE KILOMETERS ON SURFACE	
	90.0782 SQUARE KILOMETERS IN SUBSURFACE	
	114.1238 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	21.00 HOURS
	28.4820 SQUARE KILOMETERS ON SURFACE	
	105.1769 SQUARE KILOMETERS IN SUBSURFACE	
	133.6589 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	24.00 HOURS
	33.1633 SQUARE KILOMETERS ON SURFACE	
	113.5909 SQUARE KILOMETERS IN SUBSURFACE	
	146.7542 TOTAL AREA EXTENT	
THERE ARE	9 CONCENTRATION VALUES AND 2 SPILLETTS OUT THERE AT TIME	27.00 HOURS
	38.0760 SQUARE KILOMETERS ON SURFACE	
	146.7510 SQUARE KILOMETERS IN SUBSURFACE	
	184.8270 TOTAL AREA EXTENT	

Figure VIII.-16. Output of Program PLOTAREA

AREA COVERED BY SPILL

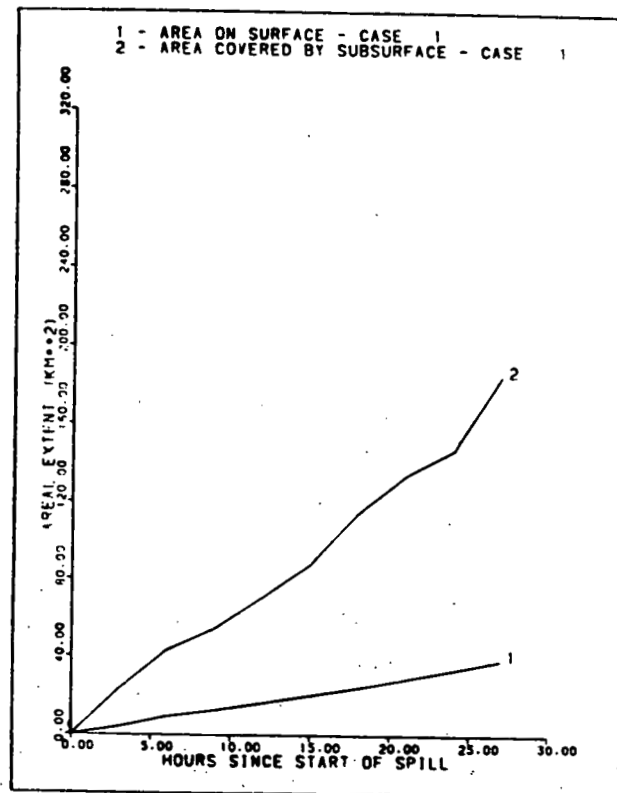


Figure VIII.-17. Plot from PLOTAREA.

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IN DEGREES X IN SECONDS
 PARTICLE PARAMETERS AT TIME 0.0

N	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION FIXED SYSTEM			PARTICLE PARAMETERS			
	X	Y	S	X	Y	S	DIAMETER	DENSITY	SPT. VBL.	WASS
1	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.9	1.001
2	0.0002	0.0002	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.9	1.001
3	0.0001	0.0001	0.6037	0.216	0.355	0.6017	0.0010	0.8770	0.0	1.001
4	0.0002	0.0002	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
5	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
6	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
7	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
8	0.0002	0.0001	0.1022	0.216	0.355	0.1022	0.0010	0.8770	0.0	1.001
9	0.0003	0.0001	0.8150	0.217	0.355	0.8150	0.0010	0.8770	0.0	1.001
10	0.0002	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
11	0.0002	0.0000	0.3865	0.216	0.355	0.3865	0.0010	0.8770	0.0	1.001
12	0.0002	0.0000	0.5872	0.216	0.355	0.5872	0.0010	0.8770	0.0	1.001
13	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
14	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
15	0.0001	0.0001	0.3554	0.216	0.355	0.3554	0.0010	0.8770	0.0	1.001
16	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
17	0.0001	0.0001	0.8167	0.216	0.355	0.8167	0.0010	0.8770	0.0	1.001
18	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
19	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
20	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
21	0.0000	0.0002	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
22	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
23	0.0002	0.0001	0.3918	0.216	0.355	0.3918	0.0010	0.8770	0.0	1.001
24	0.0002	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
25	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
26	0.0002	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
27	0.0002	0.0001	0.8150	0.217	0.355	0.8150	0.0010	0.8770	0.0	1.001
28	0.0002	0.0002	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
29	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
30	0.0002	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
31	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
32	0.0002	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
33	0.0002	0.0001	0.8150	0.217	0.355	0.8150	0.0010	0.8770	0.0	1.001
34	0.0001	0.0001	0.1608	0.216	0.355	0.1608	0.0010	0.8770	0.0	1.001
35	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
36	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001
37	0.0002	0.0002	0.5810	0.216	0.355	0.5810	0.0010	0.8770	0.0	1.001
38	0.0001	0.0001	0.8150	0.216	0.355	0.8150	0.0010	0.8770	0.0	1.001

CONCENTRATIONS AT TIME 3.00 HOURS
 WITH NEW GRID NUMBER OF GRID OF 10 10 AND 1 FOR X, Y, AND S.

FLOATING GRID SEPARATION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.2013, 0.3193) IN DEGREES WITH RESPECT TO THE ORIGIN OF THE FIXED DEPTH GRID
 THE NEW GRID SEPARATION IN THE FLOATING SYSTEM IS 0.006971400DEGREES IN X AND 0.006201200DEGREES IN Y
 THE GRID SEPARATION IN THE FIXED SYSTEM IS 0.03600DEGREES IN X AND 0.01600DEGREES IN Y
 THE AVERAGE VALUES OF X, Y AND S ARE 0.019016 0.030806 0.768267
 THE STANDARD DEVIATIONS ARE 0.003403 0.008971 0.123089

TIME	CONCENTRATION IN NO OF OIL PER RL OF WATER						STEP NUMBER	S	TIME	0.0	LEVEL
	0.20	0.21	0.22	0.23	0.24	0.25					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.35	0.35	0.36	0.36	
0.21	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.22	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00510	0.01970	0.0	
0.23	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00197	0.00716	0.0	
0.24	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.25	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	

TIME	CONCENTRATION IN NO OF OIL PER RL OF WATER						STEP NUMBER	S	TIME	0.0	LEVEL
	0.20	0.21	0.22	0.23	0.24	0.25					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.35	0.35	0.36	0.36	
0.21	0.0	0.00011	0.00036	0.00010	0.00015	0.00027	0.00005	0.0	0.0	0.0	
0.22	0.0	0.00000	0.00000	0.00000	0.00001	0.00002	0.00002	0.0	0.0	0.0	
0.23	0.0	0.00013	0.00015	0.00192	0.00013	0.00024	0.00018	0.01508	0.09818	0.00000	
0.24	0.0	0.00018	0.00078	0.00018	0.00065	0.00015	0.00027	0.00580	0.02815	0.00000	
0.25	0.0	0.0	0.00002	0.00005	0.00020	0.00013	0.0	0.0	0.0	0.0	
0.26	0.0	0.0	0.00000	0.00015	0.0	0.0	0.0	0.0	0.0	0.0	
0.27	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.28	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.29	0.0	0.0	0.0	0.0	0.00011	0.00015	0.0	0.0	0.0	0.0	
0.30	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0	0.0	0.0	

TIME	CONCENTRATION IN NO OF OIL PER RL OF WATER						STEP NUMBER	S	TIME	0.0	LEVEL
	0.20	0.21	0.22	0.23	0.24	0.25					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.35	0.35	0.36	0.36	
0.21	0.0	0.00159	0.01136	0.30968	0.00495	0.00858	0.00160	0.0	0.0	0.0	
0.22	0.0	0.00000	0.00000	0.00135	0.00017	0.00196	0.00071	0.0	0.0	0.0	
0.23	0.0	0.00001	0.00095	0.11803	0.00819	0.00818	0.00568	0.07538	0.54635	0.00000	
0.24	0.0	0.01098	0.02110	0.08782	0.02086	0.00879	0.00870	0.02675	0.11173	0.00000	
0.25	0.0	0.0	0.00005	0.00168	0.00008	0.00015	0.0	0.0	0.0	0.0	
0.26	0.0	0.0	0.00101	0.01126	0.0	0.0	0.0	0.0	0.0	0.0	
0.27	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.28	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
0.29	0.0	0.0	0.0	0.00163	0.01132	0.0	0.0	0.0	0.0	0.0	
0.30	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0	0.0	0.0	

Figure VIII.-18. Output of Program Particle

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IS DEGREES X IS RETURN
 PARTICLE PARAMETERS AT TIME 1.00

N	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION FIXED SYSTEM			DIAMETER	DENSITY	SET. VEL.	
	X	Y	Z	X	Y	Z				
1	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
2	0.0188	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
3	0.0187	0.0355	0.6017	0.220	0.355	0.6017	0.0010	0.8770	0.0	0.998
4	0.0188	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
5	0.0187	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
6	0.0187	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
7	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
8	0.0188	0.0355	0.3022	0.220	0.355	0.3022	0.0010	0.8770	0.0	0.998
9	0.0188	0.0358	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
10	0.0188	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
11	0.0188	0.0356	0.1865	0.220	0.355	0.1865	0.0010	0.8770	0.0	0.998
12	0.0188	0.0356	0.5872	0.220	0.355	0.5872	0.0010	0.8770	0.0	0.998
13	0.0187	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
14	0.0187	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
15	0.0187	0.0355	0.3550	0.220	0.355	0.3550	0.0010	0.8770	0.0	0.998
16	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
17	0.0187	0.0355	0.8167	0.220	0.355	0.8167	0.0010	0.8770	0.0	0.998
18	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
19	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
20	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
21	0.0186	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
22	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
23	0.0188	0.0355	0.1918	0.220	0.355	0.1918	0.0010	0.8770	0.0	0.998
24	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
25	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
26	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
27	0.0188	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
28	0.0188	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
29	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
30	0.0188	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
31	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
32	0.0188	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
33	0.0188	0.0356	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
34	0.0187	0.0355	0.3608	0.220	0.355	0.3608	0.0010	0.8770	0.0	0.998
35	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
36	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
37	0.0188	0.0355	0.5810	0.220	0.355	0.5810	0.0010	0.8770	0.0	0.998
38	0.0187	0.0355	0.8150	0.220	0.355	0.8150	0.0010	0.8770	0.0	0.998
39	0.0178	0.0368	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
40	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
41	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
42	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
43	0.0210	0.0068	0.8150	0.222	0.356	0.8150	0.0010	1.0032	0.0	1.001
44	0.0266	0.0207	0.8150	0.229	0.360	0.8150	0.0010	1.0032	0.0	1.001
45	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
46	0.0090	0.0282	0.8150	0.210	0.368	0.8150	0.0010	1.0032	0.0	1.001
47	0.0179	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
48	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
49	0.0075	0.0097	0.8150	0.209	0.379	0.8150	0.0010	1.0032	0.0	1.001
50	0.0180	0.0360	0.8150	0.219	0.356	0.8150	0.0010	1.0032	0.0	1.001
51	0.0208	0.0277	0.8150	0.222	0.367	0.8150	0.0010	1.0032	0.0	1.001
52	0.0211	0.0355	0.8150	0.222	0.355	0.8150	0.0010	1.0032	0.0	1.001
53	0.0226	0.0158	0.8150	0.229	0.335	0.8150	0.0010	1.0032	0.0	1.001
54	0.0211	0.0356	0.8150	0.222	0.355	0.8150	0.0010	1.0032	0.0	1.001
55	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
56	0.0180	0.0362	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
57	0.0190	0.0226	0.8150	0.220	0.362	0.8150	0.0010	1.0032	0.0	1.001
58	0.0179	0.0361	0.5717	0.219	0.356	0.5717	0.0010	0.8770	0.0	0.998
59	0.0123	0.0182	0.8150	0.248	0.318	0.8150	0.0010	1.0032	0.0	1.001
60	0.0217	0.0351	0.8150	0.221	0.356	0.8150	0.0010	1.0032	0.0	1.001
61	0.0076	0.0168	0.8150	0.209	0.376	0.8150	0.0010	1.0032	0.0	1.001
62	0.0179	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
63	0.0199	0.0120	0.8150	0.221	0.331	0.8150	0.0010	1.0032	0.0	1.001
64	0.0171	0.0181	0.8150	0.231	0.311	0.8150	0.0010	1.0032	0.0	1.001
65	0.0209	0.0187	0.8150	0.222	0.336	0.8150	0.0010	1.0032	0.0	1.001
66	0.0226	0.0179	0.8150	0.228	0.332	0.8150	0.0010	1.0032	0.0	1.001
67	0.0180	0.0362	0.8786	0.219	0.356	0.8786	0.0010	0.8770	0.0	0.998
68	0.0205	0.0187	0.7611	0.227	0.318	0.7611	0.0010	1.0032	0.0	1.001
69	0.0219	0.0171	0.8150	0.221	0.316	0.8150	0.0010	1.0032	0.0	1.001
70	0.0206	0.0178	0.8150	0.227	0.312	0.8150	0.0010	1.0032	0.0	1.001
71	0.0226	0.0168	0.8150	0.228	0.318	0.8150	0.0010	1.0032	0.0	1.001
72	0.0179	0.0368	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
73	0.0179	0.0361	0.7679	0.219	0.356	0.7679	0.0010	0.8770	0.0	0.998
74	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
75	0.0180	0.0361	0.7887	0.219	0.356	0.7887	0.0010	0.8770	0.0	0.998
76	0.0179	0.0368	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
77	0.0179	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
78	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
79	0.0179	0.0361	0.7275	0.219	0.356	0.7275	0.0010	0.8770	0.0	0.998
80	0.0179	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
81	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
82	0.0180	0.0361	0.8150	0.219	0.356	0.8150	0.0010	0.8770	0.0	0.998
83	0.0180	0.0361	0.7111	0.219	0.356	0.7111	0.0010	0.8770	0.0	0.998

Figure VIII.-18. Output of Particle

CONCENTRATIONS BY TIME 4.00 HOURS
 WITH MAX NUMBER OF GRIDS OF 10 10 AND 1 FOR X, Y, AND Z.

MOVING GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1989, 0.2932) IN DEGREES WITH RESPECT TO THE ORIGIN OF THE FIXED DEPTH GRID
 THE X-Z GRID SEPARATION IN THE FLOATING SYSTEM IS 0.0034630000000000 IN X AND 0.0068256000000000 IN Y
 THE GRID SEPARATION IN THE FIXED SYSTEM IS 0.0360000000000000 IN X AND 0.0360000000000000 IN Y
 THE AVERAGE VALUES OF X, Y AND Z ARE 0.020816 0.049768 0.766389
 THE STANDARD DEVIATIONS ARE 0.004572 0.012019 0.130512

	CONCENTRATION IN NO OF OIL PER ML OF WATER										STEP NUMBER	2	TIME	0.0	LEVEL
	0.30	0.30	0.31	0.32	0.32	0.33	0.34	0.34	0.35	0.36					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0					
0.21	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0					
0.21	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00000	0.00003	0.0				
0.22	0.0	0.0	0.0	0.0	0.0	0.0	0.00136	0.00272	0.00242	0.01544	0.0				
0.22	0.0	0.0	0.0	0.0	0.0	0.0	0.00111	0.00226	0.00022	0.00137	0.0				
0.23	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0				
0.23	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0				
0.24	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0				
0.25	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0				
0.25	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0				

	CONCENTRATION IN NO OF OIL PER ML OF WATER										STEP NUMBER	2	TIME	0.0	LEVEL
	0.30	0.30	0.31	0.32	0.32	0.33	0.34	0.34	0.35	0.36					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0					
0.21	0.0	0.0	0.0	0.0	0.00002	0.00026	0.00025	0.00016	0.00003	0.0					
0.21	0.0	0.0	0.0	0.0	0.00000	0.00002	0.00012	0.00008	0.00004	0.00240	0.00000				
0.22	0.0	0.00008	0.00144	0.00079	0.00061	0.00191	0.00079	0.00692	0.06572	0.00000					
0.22	0.0	0.00013	0.00098	0.00033	0.00060	0.00208	0.00068	0.00072	0.00176	0.0					
0.23	0.0	0.0	0.00002	0.00002	0.00001	0.00018	0.00025	0.0	0.0	0.0					
0.23	0.0	0.0	0.0	0.0	0.00005	0.00024	0.00011	0.0	0.0	0.0					
0.24	0.0	0.0	0.0	0.0	0.0	0.00001	0.00004	0.0	0.0	0.0					
0.25	0.0	0.0	0.0	0.0	0.0	0.00014	0.00011	0.0	0.0	0.0					
0.25	0.0	0.0	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0					

	CONCENTRATION IN NO OF OIL PER ML OF WATER										STEP NUMBER	2	TIME	0.0	LEVEL
	0.30	0.30	0.31	0.32	0.32	0.33	0.34	0.34	0.35	0.36					
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0					
0.21	0.0	0.0	0.0	0.0	0.00055	0.00030	0.00789	0.00508	0.00085	0.0					
0.21	0.0	0.0	0.0	0.0	0.00000	0.00079	0.00378	0.00258	0.00051	0.01473	0.00000				
0.22	0.0	0.00010	0.00703	0.00772	0.01158	0.01659	0.01456	0.01753	0.37389	0.00000					
0.22	0.0	0.00683	0.01051	0.01069	0.01853	0.04728	0.01290	0.00670	0.01865	0.0					
0.23	0.0	0.0	0.00051	0.00059	0.00025	0.00561	0.00797	0.0	0.0	0.0					
0.23	0.0	0.0	0.0	0.0	0.0	0.00168	0.00778	0.00358	0.0	0.0					
0.24	0.0	0.0	0.0	0.0	0.0	0.00092	0.00164	0.0	0.0	0.0					
0.25	0.0	0.0	0.0	0.0	0.0	0.00015	0.00019	0.0	0.0	0.0					
0.25	0.0	0.0	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0					

Figure VIII.-18. Output of Particle

PARTICLE POSITIONS X AND Y IN THE FLOPPING SYSTEM IN DECIMETRS X 10 METERS
 PARTICLE PARAMETERS AT TIME 6.00

ID	PARTICLE POSITION FLOPPING SYSTEM			PARTICLE POSITION PIPED SYSTEM			PARTICLE PARAMETERS			
	X	Y	Z	X	Y	Z	DIAMETER	DENSITY	SET. VOL.	CLASS
1	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
2	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
3	0.0196	0.0571	0.8037	0.218	0.350	0.8037	0.0010	0.8770	0.0	0.998
4	0.0196	0.0572	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
5	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
6	0.0195	0.0570	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
7	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
8	0.0196	0.0571	0.2022	0.218	0.350	0.2022	0.0010	0.8770	0.0	0.998
9	0.0197	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
10	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
11	0.0196	0.0570	0.3865	0.218	0.350	0.3865	0.0010	0.8770	0.0	0.998
12	0.0196	0.0570	0.4872	0.218	0.350	0.4872	0.0010	0.8770	0.0	0.998
13	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
14	0.0196	0.0570	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
15	0.0196	0.0571	0.3598	0.218	0.350	0.3598	0.0010	0.8770	0.0	0.998
16	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
17	0.0195	0.0571	0.8167	0.218	0.350	0.8167	0.0010	0.8770	0.0	0.998
18	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
19	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
20	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
21	0.0195	0.0572	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
22	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
23	0.0196	0.0571	0.3918	0.218	0.350	0.3918	0.0010	0.8770	0.0	0.998
24	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
25	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
26	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
27	0.0197	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
28	0.0196	0.0572	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
29	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
30	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
31	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
32	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
33	0.0197	0.0570	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
34	0.0195	0.0570	0.3608	0.218	0.350	0.3608	0.0010	0.8770	0.0	0.998
35	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
36	0.0196	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
37	0.0196	0.0571	0.5810	0.218	0.350	0.5810	0.0010	0.8770	0.0	0.998
38	0.0195	0.0571	0.8150	0.218	0.350	0.8150	0.0010	0.8770	0.0	0.998
39	0.0195	0.0580	0.8150	0.217	0.351	0.8150	0.0010	0.8770	0.0	0.998
40	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
41	0.0187	0.0579	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
42	0.0187	0.0579	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
43	0.0221	0.0277	0.8150	0.221	0.321	0.8150	0.0010	1.0012	0.0	1.001
44	0.0286	0.0822	0.8150	0.227	0.315	0.8150	0.0010	1.0012	0.0	1.001
45	0.0187	0.0579	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
46	0.0099	0.0451	0.8150	0.209	0.319	0.8150	0.0010	1.0012	0.0	1.001
47	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
48	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
49	0.0082	0.0101	0.8150	0.207	0.321	0.8150	0.0010	1.0012	0.0	1.001
50	0.0146	0.0162	0.8150	0.216	0.329	0.8150	0.0010	1.0012	0.0	1.001

Figure VIII.-18. . Output of Particle

51	0.0218	0.0890	0.8150	0.220	0.342	0.8150	0.0010	1.0032	0.0	1.001
52	0.0221	0.0168	0.8150	0.221	0.310	0.8150	0.0010	1.0032	0.0	1.001
53	0.0218	0.0172	0.8150	0.221	0.310	0.8150	0.0010	1.0032	0.0	1.001
54	0.0221	0.0165	0.8150	0.221	0.310	0.8150	0.0010	1.0032	0.0	1.001
55	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
56	0.0187	0.0579	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
57	0.0198	0.0838	0.8150	0.219	0.337	0.8150	0.0010	1.0032	0.0	1.001
58	0.0186	0.0580	0.5737	0.218	0.351	0.5717	0.0010	0.8770	0.0	0.998
59	0.0868	0.0809	0.8150	0.285	0.138	0.8150	0.0010	1.0032	0.0	1.001
60	0.0229	0.0168	0.8150	0.222	0.327	0.8150	0.0010	1.0032	0.0	1.001
61	0.0008	0.313	0.8150	0.207	0.330	0.8150	0.0010	1.0032	0.0	1.001
62	0.0186	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
63	0.0207	0.0132	0.8150	0.220	0.326	0.8150	0.0010	1.0032	0.0	1.001
64	0.0388	0.0160	0.8150	0.238	0.329	0.8150	0.0010	1.0032	0.0	1.001
65	0.0219	0.0160	0.8150	0.221	0.329	0.8150	0.0010	1.0032	0.0	1.001
66	0.0219	0.0136	0.8150	0.223	0.327	0.8150	0.0010	1.0032	0.0	1.001
67	0.0187	0.0579	0.4786	0.217	0.351	0.4786	0.0010	0.8770	0.0	0.998
68	0.0215	0.0359	0.7633	0.220	0.329	0.7613	0.0010	1.0032	0.0	1.001
69	0.0211	0.0388	0.8150	0.222	0.332	0.8150	0.0010	1.0032	0.0	1.001
70	0.0215	0.0137	0.8150	0.220	0.327	0.8150	0.0010	1.0032	0.0	1.001
71	0.0239	0.0180	0.8150	0.221	0.331	0.8150	0.0010	1.0032	0.0	1.001
72	0.0186	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
73	0.0186	0.0579	0.7679	0.217	0.351	0.7679	0.0010	0.8770	0.0	0.998
74	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
75	0.0187	0.0580	0.7887	0.218	0.351	0.7887	0.0010	0.8770	0.0	0.998
76	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
77	0.0186	0.0580	0.8150	0.217	0.351	0.8150	0.0010	0.8770	0.0	0.998
78	0.0187	0.0579	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
79	0.0186	0.0579	0.7275	0.218	0.351	0.7275	0.0010	0.8770	0.0	0.998
80	0.0186	0.0579	0.8150	0.217	0.351	0.8150	0.0010	0.8770	0.0	0.998
81	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
82	0.0187	0.0580	0.8150	0.218	0.351	0.8150	0.0010	0.8770	0.0	0.998
83	0.0187	0.0579	0.7111	0.218	0.351	0.7111	0.0010	0.8770	0.0	0.998
84	0.0211	0.0188	0.8150	0.220	0.330	0.8150	0.0010	0.9952	0.0	0.998
85	0.0218	0.0182	0.8150	0.221	0.303	0.8150	0.0010	1.0095	0.0	1.069
86	0.0252	0.0207	0.8150	0.228	0.318	0.8150	0.0010	1.0095	0.0	1.069
87	0.0216	0.0211	0.8150	0.222	0.318	0.8150	0.0010	1.0095	0.0	1.069
88	0.0210	0.0180	0.7399	0.220	0.309	0.7399	0.0010	1.0095	0.0	1.069
89	0.0250	0.0815	0.8150	0.228	0.315	0.8150	0.0010	0.9952	0.0	0.998
90	0.0211	0.0131	0.8150	0.220	0.307	0.8150	0.0010	1.0095	0.0	1.069
91	0.0187	0.0806	0.8150	0.218	0.318	0.8150	0.0010	0.9952	0.0	0.998
92	0.0216	0.0821	0.2013	0.221	0.315	0.2013	0.0010	0.9952	0.0	0.998
93	0.0281	0.0856	0.8150	0.223	0.318	0.8150	0.0010	0.9952	0.0	0.998
94	0.0172	0.0819	0.8150	0.236	0.315	0.8150	0.0010	0.9952	0.0	0.998

CONCENTRATIONS AT TIME 9.00 HOURS
WITH NEW MAX NUMBER OF GRID OF 10 AND 3 POS X, Y, AND Z.

ELONGATED GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1968, 0.2885) IN DEGREES WITH RESPECT TO THE ORIGIN OF THE FIXED DEPTH GRID
THE NEW GRID DEFINITION IN THE FLOATING SYSTEM IS 0.0059820 DEGREES IN X AND 0.0068403 DEGREES IN Y
THE GRID DEFINITION IN THE FIXED SYSTEM IS 0.0368 DEGREES IN X AND 0.0360 DEGREES IN Y

THE AVERAGE VALUES OF X, Y AND Z ARE 0.022198 0.088696 0.755368
THE STANDARD DEVIATIONS ARE 0.006793 0.012580 0.142089

CONCENTRATION IN MG OF OIL PER ML OF WATER										STEP NUMBER	J	TIME	0.0	LEVEL
0.20	0.0	0.0	0.31	0.31	0.32	0.33	0.33	0.33	0.38	0.35	0.35			
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0			
0.21	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0			
0.21	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0			
0.22	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00190	0.00321	0.00210	0.0138	0.0		
0.22	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00061	0.00106	0.0	0.0	0.0		
0.23	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00081	0.00180	0.0	0.0	0.0		
0.24	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.00115	0.00229	0.0	0.0	0.0		
0.24	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0		
0.25	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0		
0.25	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0		

CONCENTRATION IN MG OF OIL PER ML OF WATER										STEP NUMBER	J	TIME	0.0	LEVEL
0.20	0.0	0.0	0.31	0.31	0.32	0.33	0.33	0.33	0.38	0.35	0.35			
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0			
0.21	0.0	0.0	0.0	0.0	0.00005	0.00023	0.00020	0.00016	0.00001	0.0	0.0			
0.21	0.0	0.0	0.0	0.0	0.00000	0.00008	0.00018	0.00012	0.00008	0.01282	0.00000			
0.22	0.0	0.00063	0.00172	0.00025	0.00090	0.00216	0.00085	0.00602	0.05107	0.00000				
0.22	0.0	0.00016	0.00085	0.00032	0.00037	0.00120	0.00061	0.00010	0.0	0.0				
0.23	0.0	0.0	0.0	0.0	0.00001	0.00088	0.00601	0.0	0.0	0.0				
0.24	0.0	0.0	0.0	0.0	0.00003	0.00688	0.00885	0.1	0.0	0.0				
0.24	0.0	0.0	0.00018	0.00005	0.0	0.00002	0.00005	0.0	0.0	0.0				
0.25	0.0	0.0	0.00001	0.00016	0.00008	0.00007	0.00016	0.0	0.0	0.0				
0.25	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0	0.0	0.0				

CONCENTRATION IN MG OF OIL PER ML OF WATER										STEP NUMBER	J	TIME	0.0	LEVEL
0.20	0.0	0.0	0.31	0.31	0.32	0.33	0.33	0.33	0.38	0.35	0.35			
0.20	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0			
0.21	0.0	0.0	0.0	0.0	0.00186	0.00736	0.00631	0.00508	0.00036	0.0	0.0			
0.21	0.0	0.0	0.0	0.00000	0.00183	0.00571	0.00188	0.00055	0.07501	0.00000				
0.22	0.0	0.01054	0.00903	0.00815	0.02010	0.08422	0.14480	0.11151	0.28490	0.00000				
0.22	0.0	0.00186	0.00716	0.01018	0.00919	0.02908	0.1601	0.00108	0.0	0.0				
0.23	0.0	0.0	0.0	0.0	0.00025	0.00511	0.00607	0.0	0.0	0.0				
0.24	0.0	0.0	0.0	0.0	0.00089	0.00679	0.00418	0.0	0.0	0.0				
0.24	0.0	0.0	0.00568	0.00165	0.0	0.00058	0.00158	0.0	0.0	0.0				
0.25	0.0	0.0	0.00033	0.00527	0.00258	0.00219	0.00517	0.0	0.0	0.0				
0.25	0.0	0.0	0.0	0.00000	0.00000	0.0	0.0	0.0	0.0	0.0				

Figure VIII.-18. Output of Particle

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IN DEGREES X IN METERS
 PARTICLE PARAMETERS AT TIME 9.00

ID	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION PIED SYSTEM			DIAMETER	PARTICLE PARAMETERS		
	X	Y	Z	X	Y	Z		DENSITY	SUP. VEL.	BASE
1	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
2	0.0203	0.0573	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
3	0.0202	0.0572	0.6037	0.217	0.386	0.6037	0.0010	0.8770	0.0	0.998
4	0.0202	0.0573	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
5	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
6	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
7	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
8	0.0202	0.0572	0.1022	0.217	0.386	0.1022	0.0010	0.8770	0.0	0.998
9	0.0204	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
10	0.0202	0.0571	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
11	0.0203	0.0571	0.3865	0.217	0.386	0.3865	0.0010	0.8770	0.0	0.998
12	0.0203	0.0571	0.5872	0.217	0.386	0.5872	0.0010	0.8770	0.0	0.998
13	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
14	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
15	0.0202	0.0572	0.3558	0.217	0.386	0.3558	0.0010	0.8770	0.0	0.998
16	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
17	0.0202	0.0572	0.8167	0.217	0.386	0.8167	0.0010	0.8770	0.0	0.998
18	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
19	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
20	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
21	0.0201	0.0571	0.8150	0.216	0.386	0.8150	0.0010	0.8770	0.0	0.998
22	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
23	0.0202	0.0572	0.3918	0.217	0.386	0.3918	0.0010	0.8770	0.0	0.998
24	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
25	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
26	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
27	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
28	0.0202	0.0571	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
29	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
30	0.0201	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
31	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
32	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
33	0.0203	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
34	0.0201	0.0572	0.3608	0.217	0.386	0.3608	0.0010	0.8770	0.0	0.998
35	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
36	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
37	0.0201	0.0573	0.5810	0.217	0.386	0.5810	0.0010	0.8770	0.0	0.998
38	0.0202	0.0572	0.8150	0.217	0.386	0.8150	0.0010	0.8770	0.0	0.998
39	0.0180	0.0581	0.8150	0.215	0.387	0.8150	0.0010	0.8770	0.0	0.998
40	0.0182	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
41	0.0182	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
42	0.0182	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
43	0.0228	0.0276	0.8150	0.219	0.316	0.8150	0.0010	1.0032	0.0	1.001
44	0.0108	0.0822	0.8150	0.221	0.311	0.8150	0.0010	1.0032	0.0	1.001
45	0.0182	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
46	0.0108	0.0889	0.8150	0.207	0.313	0.8150	0.0010	1.0032	0.0	1.001
47	0.0182	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
48	0.0181	0.0581	0.8150	0.216	0.387	0.8150	0.0010	0.8770	0.0	0.998
49	0.0080	0.0298	0.8150	0.205	0.318	0.8150	0.0010	1.0032	0.0	1.001
50	0.0169	0.0158	0.8150	0.211	0.328	0.8150	0.0010	1.0032	0.0	1.001

Figure VIII.-18. Output of Particle

51	0.0223	0.0690	0.0150	0.219	0.337	0.0150	0.0010	1.0032	0.0	1.001
52	0.0270	0.0167	0.0150	0.219	0.325	0.0150	0.0010	1.0032	0.0	1.001
53	0.0240	0.0171	0.0150	0.221	0.326	0.0150	0.0010	1.0032	0.0	1.001
54	0.0229	0.0167	0.0150	0.219	0.325	0.0150	0.0010	1.0032	0.0	1.001
55	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
56	0.0192	0.0580	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
57	0.0201	0.0416	0.0150	0.217	0.332	0.0150	0.0010	1.0032	0.0	1.001
58	0.0191	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
59	0.0507	0.0823	0.0150	0.207	0.311	0.0150	0.0010	1.0032	0.0	1.001
60	0.0217	0.0163	0.0150	0.220	0.325	0.0150	0.0010	1.0032	0.0	1.001
61	0.0093	0.0167	0.0150	0.206	0.325	0.0150	0.0010	1.0032	0.0	1.001
62	0.0191	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
63	0.0216	0.0111	0.0150	0.210	0.322	0.0150	0.0010	0.8770	0.0	0.990
64	0.0176	0.0166	0.0150	0.230	0.325	0.0150	0.0010	1.0032	0.0	1.001
65	0.0227	0.0150	0.0150	0.219	0.320	0.0150	0.0010	1.0032	0.0	1.001
66	0.0244	0.0116	0.0150	0.221	0.322	0.0150	0.0010	1.0032	0.0	1.001
67	0.0192	0.0580	0.0150	0.216	0.306	0.0150	0.0010	0.8770	0.0	0.990
68	0.0222	0.0150	0.0150	0.219	0.326	0.0150	0.0010	1.0032	0.0	1.001
69	0.0281	0.0183	0.0150	0.221	0.327	0.0150	0.0010	1.0032	0.0	1.001
70	0.0223	0.0135	0.0150	0.219	0.322	0.0150	0.0010	1.0032	0.0	1.001
71	0.0250	0.0179	0.0150	0.221	0.326	0.0150	0.0010	1.0032	0.0	1.001
72	0.0181	0.0581	0.0150	0.215	0.307	0.0150	0.0010	0.8770	0.0	0.990
73	0.0180	0.0581	0.0150	0.215	0.307	0.0150	0.0010	0.8770	0.0	0.990
74	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
75	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
76	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
77	0.0191	0.0581	0.0150	0.215	0.307	0.0150	0.0010	0.8770	0.0	0.990
78	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
79	0.0191	0.0580	0.0150	0.215	0.307	0.0150	0.0010	0.8770	0.0	0.990
80	0.0191	0.0580	0.0150	0.215	0.307	0.0150	0.0010	0.8770	0.0	0.990
81	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
82	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
83	0.0192	0.0581	0.0150	0.216	0.307	0.0150	0.0010	0.8770	0.0	0.990
84	0.0210	0.0196	0.0150	0.210	0.320	0.0150	0.0010	0.9952	0.0	0.950
85	0.0227	0.0103	0.0150	0.219	0.290	0.0150	0.0010	1.0095	0.0	1.069
86	0.0266	0.0200	0.0150	0.221	0.308	0.0150	0.0010	1.0095	0.0	1.069
87	0.0267	0.0211	0.0150	0.221	0.310	0.0150	0.0010	1.0095	0.0	1.069
88	0.0210	0.0159	0.0150	0.210	0.308	0.0150	0.0010	1.0095	0.0	1.069
89	0.0109	0.0416	0.0150	0.227	0.310	0.0150	0.0010	0.9952	0.0	0.950
90	0.0221	0.0133	0.0150	0.219	0.302	0.0150	0.0010	1.0095	0.0	1.069
91	0.0190	0.0403	0.0150	0.219	0.329	0.0150	0.0010	0.9952	0.0	0.950
92	0.0220	0.0419	0.0150	0.219	0.310	0.0150	0.0010	0.9952	0.0	0.950
93	0.0251	0.0455	0.0150	0.222	0.310	0.0150	0.0010	0.9952	0.0	0.950
94	0.0000	0.0426	0.0150	0.237	0.311	0.0150	0.0010	0.9952	0.0	0.950
95	0.0210	0.0259	0.0150	0.219	0.310	0.0150	0.0010	1.0105	0.0	0.999
96	0.0181	0.0427	0.0150	0.211	0.311	0.0150	0.0010	1.0002	0.0	0.981
97	0.0509	0.0262	0.0150	0.207	0.315	0.0150	0.0010	1.0105	0.0	0.999
98	0.0452	0.0186	0.0150	0.202	0.307	0.0150	0.0010	1.0105	0.0	0.999
99	0.0360	0.0411	0.0150	0.231	0.310	0.0150	0.0010	1.0002	0.0	0.981
100	0.0267	0.0455	0.0150	0.223	0.310	0.0150	0.0010	1.0002	0.0	0.981
101	0.0160	0.0413	0.0150	0.211	0.310	0.0150	0.0010	1.0002	0.0	0.981
102	0.0361	0.0413	0.0150	0.232	0.310	0.0150	0.0010	1.0002	0.0	0.981

CONCENTRATIONS AT TIME 12.00 HOURS
 SITE SEE MAP NUMBER OF GRIDS OF 10 10 AND 1 FOR X, Y, AND Z.

FLOATING GRID DEFINITION AND PARTICLE LOCATION STATISTICS

ORIGIN OF FLOATING GRID IS AT (0.1922, 0.2039) IN DEGREES WITH RESPECT TO THE ORIGIN OF THE FIXED REFER GRID
 THE NEW GRID SEPARATION IN THE FLOATING SYSTEM IS 0.0078053DEGREES IN X AND 0.0068375DEGREES IN Y
 THE GRID SEPARATION IN THE FIXED SYSTEM IS 0.036DEGREES IN X AND 0.036DEGREES IN Y
 THE AVERAGE VALUES OF X, Y AND Z ARE 0.026467 0.008125 0.753847
 THE STANDARD DEVIATIONS ARE 0.010606 0.012565 0.102007

CONCENTRATION IN MG OF OIL PER ML OF WATER	STEP NUMBER	TIME	LEVEL
0.20	0.29	0.30	0.31
0.20	0.0	0.0	0.0
0.21	0.0	0.0	0.0
0.22	0.0	0.0	0.0
0.23	0.0	0.0	0.0
0.24	0.0	0.0	0.0
0.25	0.0	0.0	0.0
0.26	0.0	0.0	0.0
0.27	0.0	0.0	0.0

CONCENTRATION IN MG OF OIL PER ML OF WATER	STEP NUMBER	TIME	LEVEL
0.20	0.29	0.30	0.31
0.20	0.0	0.0	0.0
0.21	0.0	0.0	0.0
0.22	0.0	0.0	0.0
0.23	0.0	0.0	0.0
0.24	0.0	0.0	0.0
0.25	0.0	0.0	0.0
0.26	0.0	0.0	0.0
0.27	0.0	0.0	0.0

CONCENTRATION IN MG OF OIL PER ML OF WATER	STEP NUMBER	TIME	LEVEL
0.20	0.29	0.30	0.31
0.20	0.0	0.0	0.0
0.21	0.0	0.0	0.0
0.22	0.0	0.0	0.0
0.23	0.0	0.0	0.0
0.24	0.0	0.0	0.0
0.25	0.0	0.0	0.0
0.26	0.0	0.0	0.0
0.27	0.0	0.0	0.0

Figure VIII.-18. Output of Particle

PARTICLE POSITIONS X AND Y IN THE FLOATING SYSTEM IN DEGREES X IN SYSTEMS
PARTICLE PARAMETERS AT TIME 12.00

#	PARTICLE POSITION FLOATING SYSTEM			PARTICLE POSITION FIXED SYSTEM			DIAMETER	DENSITY	SET. VEL.	WASS
	X	Y	Z	X	Y	Z				
1	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
2	0.0227	0.0573	0.8150	0.215	0.382	0.8150	0.0010	0.8770	0.0	0.998
3	0.0226	0.0572	0.6037	0.215	0.381	0.6037	0.0010	0.8770	0.0	0.998
4	0.0226	0.0573	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
5	0.0225	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
6	0.0225	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
7	0.0226	0.0572	0.8150	0.215	0.382	0.8150	0.0010	0.8770	0.0	0.998
8	0.0226	0.0572	0.3022	0.215	0.381	0.3022	0.0010	0.8770	0.0	0.998
9	0.0228	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
10	0.0226	0.0573	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
11	0.0227	0.0571	0.3865	0.215	0.381	0.3865	0.0010	0.8770	0.0	0.998
12	0.0226	0.0571	0.5972	0.215	0.381	0.5972	0.0010	0.8770	0.0	0.998
13	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
14	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
15	0.0226	0.0572	0.3558	0.215	0.381	0.3558	0.0010	0.8770	0.0	0.998
16	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
17	0.0226	0.0572	0.8167	0.215	0.381	0.8167	0.0010	0.8770	0.0	0.998
18	0.0225	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
19	0.0224	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
20	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
21	0.0225	0.0573	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
22	0.0225	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
23	0.0226	0.0572	0.3938	0.215	0.381	0.3938	0.0010	0.8770	0.0	0.998
24	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
25	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
26	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
27	0.0227	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
28	0.0226	0.0573	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
29	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
10	0.0227	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
11	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
12	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
13	0.0227	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
14	0.0225	0.0572	0.3608	0.215	0.381	0.3608	0.0010	0.8770	0.0	0.998
15	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
16	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
17	0.0227	0.0571	0.5830	0.215	0.381	0.5830	0.0010	0.8770	0.0	0.998
18	0.0226	0.0572	0.8150	0.215	0.381	0.8150	0.0010	0.8770	0.0	0.998
19	0.0215	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
40	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
41	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
42	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
43	0.0252	0.0278	0.8150	0.217	0.311	0.8150	0.0010	1.0032	0.0	1.001
44	0.0119	0.0828	0.8150	0.226	0.328	0.8150	0.0010	1.0032	0.0	1.001
45	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
46	0.0117	0.0881	0.8150	0.206	0.328	0.8150	0.0010	1.0032	0.0	1.001
47	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
48	0.0217	0.0581	0.8150	0.218	0.382	0.8150	0.0010	0.8770	0.0	0.998
49	0.0117	0.0286	0.8150	0.208	0.312	0.8150	0.0010	1.0032	0.0	1.001
50	0.0193	0.0158	0.8150	0.212	0.319	0.8150	0.0010	1.0032	0.0	1.001

Figure VIII.-18. Output of Particle

91	0.0265	0.0889	0.8150	0.217	0.137	0.8150	0.0010	1.0032	0.0	1.001
92	0.0252	0.0145	0.8150	0.217	0.120	0.8150	0.0010	1.0032	0.0	1.001
93	0.0275	0.0170	0.8150	0.220	0.121	0.8150	0.0010	1.0032	0.0	1.001
94	0.0252	0.0166	0.8150	0.217	0.120	0.8150	0.0010	1.0032	0.0	1.001
95	0.0217	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
96	0.0217	0.0580	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
97	0.0226	0.0818	0.8150	0.215	0.127	0.8150	0.0010	1.0032	0.0	1.001
98	0.0216	0.0581	0.5737	0.218	0.182	0.5717	0.0010	0.8770	0.0	0.998
99	0.0569	0.0816	0.8150	0.289	0.127	0.8150	0.0010	1.0032	0.0	1.001
100	0.0261	0.0161	0.8150	0.218	0.120	0.8150	0.0010	1.0032	0.0	1.001
101	0.0121	0.0159	0.8150	0.208	0.120	0.8150	0.0010	1.0032	0.0	1.001
102	0.0216	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
103	0.0235	0.0128	0.8150	0.216	0.117	0.8150	0.0010	1.0032	0.0	1.001
104	0.0821	0.0172	0.8150	0.218	0.121	0.8150	0.0010	1.0032	0.0	1.001
105	0.0289	0.0157	0.8150	0.217	0.120	0.8150	0.0010	1.0032	0.0	1.001
106	0.0275	0.0199	0.8150	0.220	0.117	0.8150	0.0010	1.0032	0.0	1.001
107	0.0217	0.0580	0.8786	0.218	0.182	0.8786	0.0010	0.8770	0.0	0.998
108	0.0283	0.0156	0.7633	0.217	0.119	0.7633	0.0010	1.0032	0.0	1.001
109	0.0266	0.0182	0.8150	0.219	0.122	0.8150	0.0010	1.0032	0.0	1.001
110	0.0288	0.0113	0.8150	0.217	0.117	0.8150	0.0010	1.0032	0.0	1.001
111	0.0276	0.0178	0.8150	0.220	0.122	0.8150	0.0010	1.0032	0.0	1.001
112	0.0216	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
113	0.0215	0.0580	0.7679	0.218	0.182	0.7679	0.0010	0.8770	0.0	0.998
114	0.0217	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
115	0.0217	0.0581	0.7887	0.218	0.182	0.7887	0.0010	0.8770	0.0	0.998
116	0.0216	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
117	0.0216	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
118	0.0217	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
119	0.0216	0.0580	0.7275	0.218	0.182	0.7275	0.0010	0.8770	0.0	0.998
120	0.0215	0.0580	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
121	0.0217	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
122	0.0217	0.0581	0.8150	0.218	0.182	0.8150	0.0010	0.8770	0.0	0.998
123	0.0217	0.0580	0.7111	0.218	0.182	0.7111	0.0010	0.8770	0.0	0.998
124	0.0280	0.0198	0.8150	0.216	0.123	0.8150	0.0010	0.9952	0.0	0.998
125	0.0250	0.0103	0.8150	0.217	0.208	0.8150	0.0010	1.0095	0.0	1.069
126	0.0298	0.0209	0.8150	0.222	0.105	0.8150	0.0010	1.0095	0.0	1.069
127	0.0272	0.0710	0.8150	0.219	0.105	0.8150	0.0010	1.0095	0.0	1.069
128	0.0280	0.0158	0.7399	0.216	0.100	0.7399	0.0010	1.0095	0.0	1.069
129	0.0188	0.0418	0.8150	0.227	0.129	0.8150	0.0010	0.9952	0.0	0.998
130	0.0288	0.0132	0.8150	0.217	0.297	0.8150	0.0010	1.0095	0.0	1.069
131	0.0213	0.0800	0.8150	0.218	0.128	0.8150	0.0010	0.9952	0.0	0.998
132	0.0286	0.0817	0.2013	0.217	0.126	0.2013	0.0010	0.9952	0.0	0.998
133	0.0280	0.0858	0.8150	0.220	0.129	0.8150	0.0010	0.9952	0.0	0.998
134	0.0858	0.0813	0.8150	0.238	0.127	0.8150	0.0010	0.9952	0.0	0.998
135	0.0253	0.0277	0.8150	0.218	0.110	0.8150	0.0010	1.0105	0.0	0.998
136	0.0808	0.0811	0.1215	0.213	0.127	0.1215	0.0010	1.0002	0.0	0.981
137	0.0569	0.0277	0.8150	0.289	0.112	0.8150	0.0010	1.0105	0.0	0.999
138	0.0507	0.0198	0.8150	0.283	0.108	0.8150	0.0010	1.0105	0.0	0.999
139	0.0812	0.0817	0.5017	0.213	0.126	0.5017	0.0010	1.0002	0.0	0.981
140	0.0286	0.0855	0.8150	0.222	0.129	0.8150	0.0010	1.0002	0.0	0.981
141	0.0811	0.0817	0.8118	0.213	0.126	0.8118	0.0010	1.0002	0.0	0.981
142	0.0803	0.0817	0.5097	0.213	0.126	0.5097	0.0010	1.0002	0.0	0.981
143	0.0863	0.0811	0.8150	0.259	0.122	0.8150	0.0010	1.0018	0.0	0.993
144	0.0882	0.0508	0.8150	0.256	0.118	0.8150	0.0010	1.0018	0.0	0.993
145	0.0518	0.0278	0.6953	0.286	0.108	0.6953	0.0010	1.0112	0.0	1.086
146	0.0898	0.0183	0.8150	0.252	0.118	0.8150	0.0010	1.0112	0.0	1.086
147	0.0178	0.0170	0.8150	0.210	0.121	0.8150	0.0010	1.0018	0.0	0.993
148	0.0835	0.0877	0.8153	0.256	0.112	0.8153	0.0010	1.0018	0.0	0.993

Figure VIII.-18. Output of Particle

APPENDIX IX, OIL PROPERTIES

Estimated Percent Weight

Fraction	Description	Venezuelan Crude 1	Nigerian Crude 1	#2 Fuel 1	Bunker C 1	Kuwait Crude 2
1	Paraffin C ₆ -C ₁₂	10	15	10	0	5
2	Paraffin	8	15	25	1	10
3	Cycloparaffin C ₆ -C ₁₂	15	20	15	0	11
4	Cycloparaffin C ₁₃ -C ₂₃	20	20	15	1	5
5	Aromatic Mono- and Di-Cyclic C ₆ -C ₁₁	5	5	15	0	10
6	Aromatic Polycyclic C ₁₂ -C ₁₈	2	3	5	1	08
7	Naphtheno- Aromatic C ₉ -C ₂₅	15	7	15	1	21
8	Residual	25	15	0	96	30
	Specific Gravity	.8769	.8446	.8472	1.019	0.867

References for Oil Properties

1. Wang et al. (1976)
2. Persen (1979), approximated composition from this data.

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12.4 Section 6 Appendices

- 12.4.1 Appendix A Advective Currents for Computer Model
- 12.4.2 Appendix B Oil Spill Fisheries Computer Program

APPENDIX A

A theoretical relationship between the variance s^2 in one dimension of a diffusing cloud and the diffusivity D is

$$s = 2Dt, \quad (1)$$

(Csanady, 1973) in which t is time. Let us assume a characteristic diffusion velocity for the cloud as a whole at the j^{th} timestep, u^j . Then in a discrete particle and time model with timestep dt , the position of the k^{th} particle at the j^{th} timestep, r_{jk} , will be the sum of all previous displacements. Incorporating the intrinsically stochastic nature of turbulence through the use of a random variate, R_{jk} , chosen from the uniform probability distribution $[-1,1]$, we have, for no bulk transport velocities,

$$r_{jk} = \sum_{\ell=1}^k R_{\ell k} * u^{\ell} * dt. \quad (2)$$

Equating (1) with the statistical definition of the variance, and performing a translation of coordinates so that the origin coincides with the center of mass of the diffusing cloud composed of N particles gives

$$2jdtD = (1/N) * \sum_{k=1}^N \left(\sum_{\ell=1}^j R_{\ell k} * u^{\ell} * dt \right)^2 \quad (3)$$

Replacing u^{ℓ} with its expected value for the given problem, $E(u^{\ell})$, and noting that

$$\left(\sum_{\ell=1}^j R_{\ell k} \right)^2 = \sum_{\ell=1}^j R_{\ell k}^2 + 2 * \sum_{\substack{i=1 \\ (i \neq \ell)}}^j \sum_{\ell=1}^j R_{ik} * R_{\ell k} \quad (4)$$

in which the double sum on the right tends to zero for large j , and further that

$$\sum_{k=1}^N \sum_{\ell=1}^j R_{\ell k}^2 = N * j / 3, \quad (5)$$

the probability density function being equal to $1/2$ on the given

interval, we have

$$E(u') = \sqrt{6*D/dt} \quad (6)$$

The value of D is then chosen from an oceanic diffusion diagram (Okubo, 1974, for example), the radius of the spawning area being used as the characteristic length. By superposition, the net transport of the k th particle during the j th timestep, dr_{jk} , is

$$dr_{jk} = (R_{jk} * E(u') + U_{jk}) * dt, \quad (7)$$

in which U_{jk} is the net advective velocity contribution.

Section 12.4 Appendix 6B

CONTENTS

- I. Program Purpose and Overview
- II. Program Component Explanation
- III. Basic User Instruction
- IV. Program Listing, with Data Sets
- V. Sample Output

I. Program Purpose and Overview

This computer program was constructed as part of a larger effort at the University of Rhode Island to investigate environmental effects of oil spill treatment strategies. The specific problem addressed here is when and whether chemical oil spill treatment with dispersants might mitigate the impacts of an offshore commercial fishery. The primary effect is assumed to occur through egg and larval mortality. This implicitly assumes that both demersal juveniles and adults will avoid contaminated areas, that the feeding and spawning cycles will not be grossly interrupted, and that the stock will not suffer through subsequent bioaccumulation. The major program components are, therefore, a population model for a unit stock fishery, an ocean transport model, and a set of subroutines designed to interface these with output from the oil spill fates model also designed as part of this project. The program has been carefully and fully described internally through comment statements. After reading this manual, any actual applications of the program to an area and/or fishery other than the Georges Bank cod stock will require a working knowledge of the program itself, a listing of which is included here as Appendix I. It is advised that no internal program changes be made until one has read through and understands the program in its entirety, since changes in one section will have second and third order manifestations elsewhere.

The following description is designed to assist in the implementation of the program for new species and physical areas. For explicit sources of information regarding parameters used in the given data sets, the user is referred to the following publications:

- Reed, M., Development and Application of a Fishery Population Dynamics Model for Environmental Impact Assessment, unpub. Ph.D. Thesis, Fall, 1979.
- Reed, M., and M.L. Spaulding, "An Oilspill-Fishery Interaction Model," Part X in Environmental Assessment of Treated Versus Untreated Oil Spills: Second Interim Progress Report, U.S. Dept. of Energy Contract No. E(11-1) 4047, 1978.
- Reed, M., and M.L. Spaulding, "An Oilspill-Fishery Interaction Model: Comparison of Treated and Untreated Spill Impacts," Proceedings of 1979 Oilspill Conference, pp. 63-73, March, 1979.
- Reed, M., M.L. Spaulding and P. Cornillon, "A Fishery-Oilspill Interaction Model: Estimated Consequences of Oil Well Blowouts," Proceedings of the NATO Symposium on Operations Research in Fisheries, Trondheim, Norway, August 1979 (in press).
- Cornillon, P., M.L. Spaulding and M. Reed, "Impact Assessment in Oil Spill Modeling," paper presented at the Workshop on the Physical Behavior of Oil in the Marine Environment, Princeton, May, 1979.

II. Program Component Explanation

1) Main

The main program contains the daily cycle elements for the population model. This is the master program from which all subroutines are called, and through which all program activities are coordinated. The program is initialized, all control variables are read in, and then the annual and daily cycles are entered. Operations continue until the specified end time is reached.

2) Subroutine COMPAR

This subroutine was designed to attempt to sort out reduction rates in numbers of larvae per unit volume due to mortality versus diffusion and transport. The day of the year for this comparison is specified as input variable IDATE. The comparison is performed in the elements read into array INTELM from data set 9.

3) Subroutine BYPASS

Program run time can be reduced by increasing variable DT2 up to 5 days. This subroutine uses this secondary timestep subsequent to the spill year in both analytical and numerical time integrations, and bypasses the daily cycle in the main program.

4) Subroutine MOROIL

If MULTI is greater than 1, and KYEAR is greater than SPILYR, this subroutine is called to assign a new spill year and oil source data set.

5) Subroutine WEIGHT

Here the statistical data for the stock at hand is used to calculate weight-at-age data. Weight is called only once from Main.

6) Subroutine AVGFEC

The average number of eggs per female is calculated here, as a check against both weight and fecundity assumptions. Output is annual.

7) Subroutine SPNTIM

The spawning distribution in time is specified here. This is the result of relatively subjective evaluations to date, since no statistical data is available.

8) Subroutine DEVELOP

This subroutine controls development of eggs and larvae according to whatever information is available.

9) Subroutine TEMP

At present a constant seasonal surface water temperature is supplied. This input can be altered in response to improved data availability.

10) Subroutine TOXIC

This subroutine interfaces the hydrocarbon concentration data; input either through SR HCCONC or HCCON2, with population model. First natural mortality effects are accounted for, followed by a check to see which, if any, organisms are within an area in which concentrations exceed that specified by THRSLD. This routine is called from MAIN directly after the input of the oil concentration data.

11) Subroutine HCCONC

For SPLTYP = 1 (an instantaneous spill), this subroutine reads in data output by the oil spill behavior model on a daily basis. Conversion from latitude and longitude to the distance units of the fish model is followed by output to data set 4 of the oil, egg, and larvae distributions at that time.

12) Subroutine OUTPUT

Here annual output is directed to the printer, and oil spill case identification data with the annual yield estimates are output to data set 8.

13) Subroutine EGGMRT

Natural mortality of both density dependent and density independent varieties is applied to the egg stages. The toxicity sections originally programmed here and in SR PLNMRT are not used.

14) Subroutine PLNMRT

Here background mortalities are applied to the three planktonic stages in the model. As with SR EGGMRT, the toxicity section is not used.

15) Subroutine BTMMRT

Here a second order Taylor expansion supplies means for a numerical solution of the juvenile mortalities, including cannibalism by adults.

16) Subroutine HATCH

This is actually only a function, which returns the number of days to hatch, given an input temperature. The call is from SR DEVELOP.

17) Subroutine SPNPLC

Here eggs to be spawned on a particular day are divided into groups, and placed at random within the spawning area. On first entry, the center and radius of the spawning area are read in from data set 9. Then

for each particle, or group, a call is made to SR RANDU, which returns a random variate used to locate the particle's initial position.

18) Subroutine HCCON2

When SPLTYP = 2 (i.e., a blowout), this SR reads in the concentration data output by the oil model (data set 3). These are then written out to data set 4 along with the current egg and larval fish distributions.

19) Subroutine DSCWRT

The first time this subroutine is called, 12 days are read into array IDAYZ from data set 16. On subsequent calls, the present modeled day is compared with the members of KDAYZ. If a match is found, the day's ichthyoplankton distribution is output to disc. Otherwise, control is returned to SR ADVDIF.

20) Subroutine ADVDIF

This subroutine, which is called from MAIN, controls the advective - dispersive section of the model. Upon first entry, the physical sector of the model is initialized through subroutines FERREAD, VAREAD, VARSET, and CHECK. Calls are then made to subroutines MOVE, DEAD, COMPRS, and DSCWRT. After the first entry, only this latter group is activated.

21) Subroutine MOVE

Advection and diffusion of particles is accomplished here. First subroutine VELIN is called, to supply the advective currents for the day in question. If the logical variable DOSPWN has a value of true, SR SPNPLC is called. Then each particle is located within an element (grid) of the physical model, and planar interpolation among the three defining nodes is applied to determine an advective contribution at the given particle location. A random walk diffusion velocity calculation follows, the result being superimposed on the advective velocity and multiplied by the model timestep to produce a physical displacement of the particle.

22) Subroutine INIT

This is a convenience subroutine, where in any arrays and variables can be initialized. In general, everything is set to zero to avoid undefined variables.

23) Subroutine FERREAD

Called once from subroutine ADVDIF, the program section reads element, node, and diffusive control parameters from data set 10. Then actual node numbers and locations (in latitude and longitude) are read in and converted. Thus, the physical reference grid is established.

24) Subroutine VELIN

Here the velocity data is read into the model from data sets 13 (long term net drifts) and 14 (wind-wave currents). The output values are the sum of these two.

25) Subroutine VAREAD

The initial particle data and random variate seed, along with output write and plot time steps are read in from data set 10. Thus, an initial particle distribution can be stipulated if desired. In addition, if a uniform drift velocity is to be applied over the entire physical field, that is input here from data set 10.

26) Subroutine DEAD

Mortality due to transport out of a favorable developmental area can be included here by setting variable IOFF = 1. Due to lack of any verification data for this process, this subroutine has not been used to date.

27) Subroutine COMPRS

In an effort to keep storage requirements to a minimum this subprogram was designed to compress arrays as particles are removed from the system. Particle attrition occurs as the result of the growth of larvae to juveniles, hydrocarbon mortality, or whenever particles are transported out of the physical domain of the model.

28) Subroutine CHECK

After input of the node and element data through SR FEREAD, this subroutine checks to confirm that the nodes associates with a given element are ordered counterclockwise. This is necessary so that, when associating a given particle with a given element, SR MOVE can simply proceed around the element counterclockwise and check to see that the particle is always to the left of the line between successive nodes.

29) Subroutine VARSET

The slope and direction of the lines connecting successive nodes are calculated here, along with adjacent elements. Storage of this information greatly decreases subsequent search time when attempting to locate particles in elements.

30) Subroutine SLPDIR

This does the actual mathematics for SR VARSET, which is primarily logical in nature.

31) Subroutine WRTOUT

This generates printed output at the desired intervals, and calls SR STATS.

32) Subroutine STATS

Here particle statistics (e.g. centroid and variance of the present distribution) are calculated. Although not employed for the full scale fishery runs, this subroutine is useful for verifying the physical system definitions, initial conditions for particle placement, and for comparing theoretical with modeled diffusion rates. Changes can be made freely in

this subroutine, so long as no common arrays and variables are revalued.

III. Basic User Instructions

There are 21 primary options built into the program. The user can, therefore, run the program in a variety of modes without altering any internal code. The options are read in by the main program from data set 9. In this data set (see end of program listing in Appendix I) the variables are explicitly labeled so that no confusion will exist. A self-explanatory list of input control variables follows.

```

1150 C*****
1160 C
1170 C LIST AND EXPLANATION OF INPUT CONTROL VARIABLES
1180 C
1190 C*****
1200 C OILCOD = 1 THEN OIL IS TRUE
1210 C       = 0 THEN OIL IS FALSE AND NO ADVECTION IS PERFORMED EVER
1220 C IOFF  = 1 THEN DELETE EGGS AND LARVAE BLOWN OFF THE BANK (SEE SR DEAD
1230 C       = 0 THEN DON'T
1240 C YEARLY = THE FIRST YEAR USING THE LARGER TIMESTEP (DT2)
1250 C       (IF SPILDA=350 OR 90 AND MULTI > 1, YEARLY IS C CALCULATED
1260 C                               INTERNALLY.)
1270 C IRWND  = 1 THEN REWIND DATASET 3 AFTER EACH SPILL AND REREAD
1280 C       = 0 THEN READ FT03F002 THE SECOND SPILL, ETC.
1290 C INTPOP = 1 THEN READ THE INITIAL POPULATION FOR YEAR ISTART FROM
1300 C       DATASET 15
1310 C       = 0 THEN READ IT FROM FT09F001 (CARDS)
1320 C OUTPOP = 1 THEN WRITE THE POPULATION OUT TO 15 FOR LASTYR
1330 C       = 0 THEN DON'T
1340 C FRSTYR = THE FIRST YEAR OF RECORDED OUTPUT
1350 C LASTYR = THE LAST ONE
1360 C ISTART = THE STARTUP YEAR
1370 C MULTI  = 1 THEN THERE'S ONLY ONE SPILL
1380 C       = GT 1, THEN THAT'S THE NUMBER OF SPILLS THERE WILL BE
1390 C OILSTP = THE NUMBER (INTEGER) OF YEARS BETWEEN SPILLS
1400 C SPILYR = THE YEAR OF THE SPILL
1410 C       (OR PERHAPS SPILYR + 1 IF IADV=1 AND SPILDA IS IN AUTUMN)
1420 C SPILDA = THE JULIAN DAY OF THE SPILL
1430 C MRTDAY = JULIAN DAY FROM WHICH TO FOLLOW EGG AND LARVAL MORTALITY
1440 C MRTYR  = THE YEAR FOR SAME...RESULTS OUTPUT TO DATASET 17
1450 C IDALST = THE LAST DAY OF ADVECTION WHEN IADV = 1
1460 C IADV   = 1 THEN WE ADVECT WITHOUT OIL (SET OILCOD = 1)
1470 C       = 0 THEN NO EFFECT
1480 C SPLTYF = 1 THEN THE PROGRAM USES SR HCCONC, AND ONLY C CHECKS THE
1490 C       EXTREMES OF THE SUBSURFACE DISTRIBUTION
1500 C       = 2 THEN USES HCCON2, AND C CHECK C ELL BY C ELL...THIS IS THE
1510 C       INPUT VALUE FOR THE BLOWOUT SIMULATION, SINCE THE PATTERN
1520 C       IS NOT EXPECTED TO BE SO NICELY REGULAR....
1530 C THRSLD = THE THRESHOLD TOXICITY VALUE AT WHICH EGGS AND LARVAE ARE
1540 C       ASSUMED TO BE KILLED (IN PARTS PER BILLION)
1550 C
1560 C ICROP  = 1 THEN ARTIFICIAL C ROPPING AT SPILYRS (INTERVAL OILSTP)
1570 C       WILL OCCUR; SET OILCOD TO 0 AND MULTI GT 1
1580 C CROPRT = THE REDUCTION RATE FOR RECRUITS WHEN ICROP=1 AND KYEAR=SPILY

```

It should be noted that every combination of control variable values will require a different amount of CPU time. The program as listed (and punched on cards) is set up to be run under WAT 5, to permit facile location of user errors. When a particular model run is seen to be operating correctly, future runs (with different threshold values, for example) can be made more rapidly by switching to the "G" or "H" compiler, or by creating a compiled load module. This latter option will also decrease core requirements from 512K to 320K, an important consideration in computer turn around time.

The data sets as included with the punched output, will simulate the population response to an oilwell blowout occurring at 66.75° W Long., 41.6° N Lat. on December 15th (Julian Day 350). The spill year is 1979, and the run will end in 2020. The secondary (rapid integration) timestep is set at 5, its maximum acceptable value. Fishing effort oscillates randomly about 25 thousand standard days per year. For verification purposes, the output of the card deck is available with the cards (2 boxes). This run should take approximately 35 minutes of CPU time at 512K.


```

C//T10,SPLYTP = 1 THEN ITS SHORT, =2 THEN A BLOWOUT, T65,14,
C//T10, THE THRESHOLD TORIET IN PARTS PER BILLION IS, T65,185,
C//T10, IS THIS AN ARTIFICIAL CREEPING RUN? (CROP) T85,14,
C//T10, CREEPING RATE FOR RECRUITS DURING SPILYK (CROPAT) T85,14,
C//T10,
805 FORMAT(4I8,EB,1)
806 FORMAT(4E12.4,EM1 = ,E12.4,EM2 = ,
807 E12.4,EM3 = ,E12.4)
808 FORMAT(7E12.4,EM4 = ,E12.4,EM5 = ,E12.4,EM6 = ,E12.4)
809 FORMAT(1,1,RATE OF FEMALES IN THE POPULATION = ,F6.4,
C//ADULT NATURAL MORTALITY = ,F6.4,
C//STARTUP FISHING MORTALITY = ,F6.4,
C//EQUILIBRIUM FISHING MORTALITY = ,F6.4,
C//SELECTIVITY COEFFICIENT = ,F6.4)
810 FORMAT(2I8,F6.4)
811 FORMAT(1,1,DELTA FOR THE FISHERY MODEL IS ,F6.4, DAYS.)
813 FORMAT(1,1,HISTOGRAMS WILL BE PRODUCED FOR YEARS,
C//14, TO ,14,.)
814 FORMAT(2I8,EB,2)
815 FORMAT(4I8,EB,2)
816 FORMAT(1,1,AGE GROUP, 4I,INITIAL NUMBERS)
817 FORMAT(1,1,THE SHORTCUT TIMESTEP IS ,F6.4, DAYS.)
818 FORMAT(1,1,4,1,4,2,1,8,1,8,1,8,1,8)
821 FORMAT(1,1,F6.4)
831 FORMAT(1,1,THERE WILL BE ,14, OILSPILLS SEPARATED BY,
C//14, YEARS EACH.,//)
C READ IN THE FISHERY MODEL TIMESTEP, AND THE SHORTCUT TIMESTEP:
C
C READ(9,810)DELTA,DT2
C WRITE(6,811)DELTA1
C WRITE(6,812)DT2
C
C SET TOXICITY MORTALITY RATES TO ZERO:
C
C 11=0.0
C 12=0.0
C 13=0.0
C 14=0.0
C
C
C DO 20 I=1,75
C VMAS(I)=0.0
C
C
C MINYR AND MAXYR ARE THE FIRST AND LAST YEARS FOR
C WHICH HISTOGRAMS WILL BE PRODUCED. (THEY WILL ALWAYS
C BE OUTPUT FOR YEAR FIRSTYR AND YEAR LASTYR.)
C
C READ(9,801)MINYR,MAXYR
C WRITE(6,813)MINYR,MAXYR
C
C
C HERE READ IN THE DAY AND THE ELEMENT NUMBERS FOR DIFFUSION
C VERSUS MORTALITY RATE COMPARISONS
C
C REAC(9,820)INTELM(I),I=1,10)
C REAC(9,820)ICATE
C WRITE(6,821)DATE
C WRITE(6,820)INTELM(I),I=1,10)
C20 FORMAT(10I4)
C22 FORMAT(1,1,HERE ARE THE ELEMENTS IN WHICH,
C//MORTALITY AND DIFFUSION RATES WILL BE COMPARED ON DAY,14)
C
C WRITE(6,803)OILCO,IOFF,YEARLY,IRWNO,INTPOP,CUIPOP,FRSTYK,
C//LASTYR,ISTART,MULTI,CILSTP,SPILYR,SPILUA
C WRITE(6,804)MRTDAY
C WRITE(6,806)IDALST,IACV,SPLYTP,THRSLD,ECROP,CROPKT
C WRITE(6,808)EM10,EM11,EM12,EM13
C WRITE(6,808)EM14,EM15,EM16
C
C INITIALIZE THE MODEL POPULATION
C
C WRITE(6,816)
C
C RXI=9
C IF(INTPOP.EQ.1)RXI=15
C DO 30 I=1,18
C IMIN=I-1
C READ(IXI,814)POPNI(I)
C IF(INTPOP.EQ.1)REAC(9,814)DUMMY
C WRITE(6,815)IMIN,PCPN(I)
C POPNE(I)=POPNI(I)
C30 POPD(I)=C.0
C
C *****
C FECUNDITY AND SELECTIVITY FACTORS
C *****
C
C READ(9,832)
C READ(9,834)(FEC(I),I=1,18)
C READ(9,834)(SEL(I),I=1,18)
C READ(9,832)
C READ(9,836)ECPRGP
C32 FORMAT(10F4,1)
C34 FORMAT(18,18F4,2)
C36 FORMAT(18,EB,3)
C
C CALL WEIGHT
C
C MTCALC(I) IS IN KG
C
C DO 40 I=1,18

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```

40 FEC(I)=FEC(I)*ECPRGP*MTCALC(I)
C
C WRITE(6,50)
50 FORMAT(1,1,20X,AGE,10X,FECUNDITY)
C
C DO 60 I=2,18
C JJ=I-1
60 WRITE(6,70)JJ,FEC(I)
70 FORMAT(20X,I2,13X,E1C.4)
C
C *****
C READ IN THE CATCH AND EFFORT DATA
C AND WRITE IT OUT THE FIRST TIME THRU
C *****
C
C WRITE(6,90)
80 FORMAT(1,1,3X,YEAR,14X,CATCH,20X,EFFORT)
90 FORMAT(18X,(10HOLS,PETRI,CICHS),3X,(10HOLS,STANDARD DAYS))
C
C DO 100 I=1,75
C READ(9,110,END=130)KYR,RLCTM(I),EFFORT(I)
C WRITE(6,120)KYR,RLCTM(I),EFFORT(I)
C IF(KYR.GE.2050)CC TC 130
100 CC=INUC
120 FORMAT(14X,I4,10X,F1C.2,15X,F10.2)
110 FORMAT(14,F5.1,F5.1)
C
C130 CC=INUC
C
C THESE ARE THE RATES OF PRECATION OF THE
C 1TH AGE GROUP ON THE FIRST YEAR GROUP
C
C READ(9,840)
C READ(9,840)(PREC(I),I=1,18)
C WRITE(6,842)
C WRITE(6,840)(PREC(I),I=1,18)
C40 FORMAT(5E8,2)
C42 FORMAT(1,1,FOLLOWING ARE THE PRECATION RATES OF THE OLDER COH,
C//CN THE JUVENILES OF THE YEAR:*)
C
C EMPTY OUT PLARVA, OR INITIALIZE LATER WHEN YOU KNOW HOW
C
C
C DO 150 I=1,365
C EGCH(I)=0.0
C DO 150 J=1,18
150 PLARVA(I,J)=0.0
C
C
C LOT=IF(IXIDELTA)
C *****
C START IN ISTART TO ACIEVE ECLM
C *****
C
C KYEAR IS THE ANNUAL COUNTER.
C *****
C *****
C
C KYEAR=ISTART
C KYEAR=KYEAR+1
C IF(MULTI.GT.1.AND.KYEAR.GT.SPILYR.AND..NOT.CIL)
C CALL MODDIL(SPILYR,MULTI,CILSTP,IRWNO)
C IF(CROP.EC.1)OIL=FALSE
C
C IF(MULTI.GT.1.AND.SPILUA.EQ.350)YEARLY=SPILYR + 2
C IF(MULTI.GT.1.AND.SPILUA.EC.60)YEARLY=SPILYR + 1
C
C KCOUNT=KYEAR-ISTART
C IF(KYEAR.LT.FRSTYR)KCOUNT=1
C
C COUNT THE RECRUITS FOR THE YEAR W/ RCTCNT
C
C RCTCNT=0.0
C
C
C DO 175 I=2,18
C IF(KYEAR.LT.1)PEPNE(I)=POPNI(I)
175 IF(KYEAR.GT.1)PEPNI(I)=PEPNE(I)
C
C WRITE THE POPULATION OUT TO DIS CFDR SYMPL PLOTS
C
C *****
C CALCULATE THE ANNUAL F
C
C IF(KYEAR.LT.FRSTYR)F=FINITL
C IF(KYEAR.LT.FRSTYR)GO TO 182
C IF(KYEAR.GT.LASTYR)F=FCLOS
C IF(KYEAR.GT.LASTYR)GO TO 182
C
C180 F=Q*EFFORT(KCOUNT)
C
C STORE THE PRESENT POPULATION SIZE

```

```

182 POPSTZRCOUNTI=0.0
DO 185 I=2,18
POPSTZRCOUNTI=POPSTZRCOUNTI+PCPNII
185 CONTINUE
CYCLE THE ADULT POPULATION
190 DO 200 I=2,18
PCPNII=PCPNII*EXP(-EM+IF*SELI(I))
EXPNTII=EXPNTI-EM-IF*SELI(I)*DELTA/365.01
200 CONTINUE
CALCULATE ANNUAL YIELD
YIELD=0.0
DO 205 I=2,18
CFF(I)=PCPNII-PCNII
WCTCALC(I)=CFF(I)*SELI(I)
YIELD=YIELD+WCTCALC(I)
205 CONTINUE
CCATCHKCOUNTI=YIELD
WRITE THIS OUT FOR THE INITIALIZATION PERIOD
208 IF (KYEAR.LT.FRSTYR) WRITE(6,2) KYEAR,YIELD
FORMAT(4X,15.4X,E10.2)
.....
CALCULATE BIOMASS B
B=0.0
DO 210 I=2,18
BYEM=PCPNII*WCTCALC(I)
B=B+BYEM
210 CONTINUE
YRBIOMASS(BCCOUNTI)=B
CALCULATE CONDITION FACTOR
CCND=1.0
CALCULATE THE SPAWN FOR THE YEAR
PCPNII=0.0
DO 215 I=2,18
PCPNII=PCPNII+((PCPNII)+PCPNW(I))/2.01*RAVIO*FECEI)*CUND
215 CONTINUE
EGGS=PCPA(I)
THE ANNUAL OUTPUT SECTION
(SKIP IT FOR THE INITIALIZATION YEARS)
IF (KYEAR.LT.FRSTYR) GO TO 216
CALL OUTPUT(YIELD,B,F,EM,KYEAR)
CALCULATE THE AVERAGE FECUNDITY
CALL AVFEC(PCPNII)
216 CONTINUE
.....
NOW ENTER THE DAILY CYCLE
.....
AFTER ADVECTION IS NO LONGER OF INTEREST, AND IF ONLY
A FEW EGGS REMAIN, WE DO THIS LITTLE
SECTION. OTHERWISE, BYPASS IT.
YEARLY IS THE FIRST YEAR OF THIS TYPE OF REGIME
.....
IF (KYEAR.LT.YEARLY) GO TO 230
CALL BYPASS(RCTCNT,EM0,EM1,EM2,EM3,EM4,EM5,EM6,
ICAT,DT2,DELTA,EM,F,KYEAR,ICROP,LRUPHT)
GO TO 400
.....
HERE FOR THE REGULAR DAILY CYCLE
230 IDAY=1
225 CONTINUE
CALCULATE TODAY'S ADULT POPULATION
DO 300 I=2,18

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300 PCPNW(I)=PCPNW(I)*EXPNT(I)
CONTINUE
THEY ALSO AGE DAILY
DO 305 I=3,18
N=20-I
J=21-I
PCPNW(I)=PCPNW(I)*DELTA/365.0
PCNEM(I)=PCPNW(I)+ADDS
PCNEM(KI)=PCPNW(KI)-ADDS
305 CONTINUE
AND NEW RECRUITS ARE ADDED
ARBITRARY FIRST YEAR RECRUITMENT
IF (KYEAR.EQ.1) RECRUT=15.06*DELTA/365.0
IF (ICROP.EQ.1) AND (KYEAR.EQ.SPILYR) RECRUT=RECRUT*CAOPRI
RCTCNT=RCTCNT+RECRUT
PCPNW(2)=PCPNW(2)+RECRUT
THE LARVAE AGE
DO 310 I=1,365,107
IF (PLARVAI(1).EQ.0) GO TO 310
PLARVAI(3)=PLARVAI(1)+DELTA
PLARVAI(4)=PLARVAI(3)+DELTA
310 CONTINUE
SPAWN DISTRIBUTION IN TIME
TYPE=FLOAT(ICAY)
CALL SPWNTIME(DELTA,DISTRB)
PLARVAI(DAY,1)=PCNII*DISTPB
PLARVAI(DAY,2)=1.0
PLARVAI(DAY,3)=0.0
PLARVAI(DAY,4)=0.0
HERE TO KEEP TRACK OF FIRST YEAR MORTALITY FOR FUTURE PLOTTING
IF (KYEAR.NE.FRSTYR) GO TO 320
IF (ICAY.NE.MP) DAYIGD TO 320
MRTDAY=MRTDAY+1
LRVDAY=LRVDAY+1
IF (MRTDAY.EQ.364) MRTYR=MRTYR+1
IF (MRTDAY.EQ.364) MRTDAY=1
WRITE(12,833) PLARVAI(MORTO,1),LRVDAY,ICAY
833 FORMAT(15.2,21.1)
IF (LRVDAY.EQ.365) MRTYR=9995
320 CONTINUE
CIRCUMVENT THE SPATIAL SECTION IF THERE'S NO SPILL.
FOR THE BASELINE CASE, GO TO 370 30 DAYS AFTER THE SPILL.
FOR THE ONE YEAR ADVECTION OF LARVAE, IADV = 1
IF (ICADV.EQ.1) GO TO 370
IF (KYEAR.LT.SPILYR) GO TO 370
IF (ICADV.EQ.1) AND (KYEAR.GT.SPILYR) IADV=FALSE
IF (ICADV.EQ.1) AND (KYEAR.EQ.SPILYR) AND (IDAY.GE.27) GO TO 355
IF (ICADV.EQ.1) AND (KYEAR.EQ.SPILYR) AND (IDAY.LE.IDALST) GO TO 355
IF (ICADV.EQ.1) GO TO 370
350 IF (ISPILDA.EQ.390) AND (KYEAR.LT.SPILYR) GO TO 370
IF (ISPILDA.EQ.390) AND (KYEAR.EQ.SPILYR)
AND (ICAY.LE.27) GO TO 370
IF (ISPILDA.EQ.90) AND (KYEAR.LT.SPILYR) GO TO 370
IF (ISPILDA.EQ.90) AND (KYEAR.EQ.SPILYR)
AND (IDAY.LT.27) GO TO 370
THAT SETS UP THE SPATIAL DISTRIBUTION FOR THE SPILL.
COME HERE IN SUBSEQUENT YEARS TO CHECK FOR OIL
IF (ISPLTYD.EQ.1) CALL MCCONC(KYEAR,ICAY)
IF (ISPLTYD.EQ.2) CALL MCCONC(KYEAR,ICAY)
IF OIL COMES BACK - TRUE, THEN THERE'S OIL OUT THERE SOMEWHERE.
FOR ALL BE!
ADVECT AND DIFFUSE EGGS AND LARVAE ALREADY PRESENT.
355 CONTINUE
IF (ICAY.EQ.1) CALL CEMPAR(ICAY,KYEAR,INTELM)
360 CALL ADVDTF(IDAY,MPHAX,ICFF)
IF (ICAY.EQ.1) CALL CEMPAR(ICAY,KYEAR,INTELM)
SPAWN DISTRIBUTION IN SPACE IS ACCOMPLISHED BY SR SPWPLC.
CALLED FROM SR MOVE.
CALL TOXIC(STAGE,ICAY)

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```

.....
EGG, LARVAL, AND JUVENILE MORTALITY
370 CALL EGGMRT(EM10,EM11,T1,T2,ICAY,DELTAT)
C
SUMPN=0.0
DD 380 I=2,18
SUMPN=SUMPN + (PRED(I)*PGPNEW(I))
380 CONTINUE
C
CALL PLNMRT(EM12,EM13,T3,T4,1DAY,DELTAT)
C
Z=EM*F
C
CALL DIMMRT(Z,EM14,EM15,EM16,ICAY,DELTAT)
IF(1DAY.EQ.1)DATECALL COPPAR(1CAY,KYEAR,INTELM)
C
NOW THEY DEVELOPE
390 CALL DEVELP(1DAY,RECRUT)
C
THIS IS THE END OF THE DAILY CYCLE
1DAY=1CAY + LDT
IF(1DAY.LT.365)GOTO 225
C
.....
400 CONTINUE
C
IF(KYEAR.LT.FRSTYR)GOTO 170
IF(KYEAR.EQ.FRSTYR)GOTO 958
IF(KYEAR.EQ.LASTYR)GOTO 958
IF(KYEAR.LT.MINYR)GOTO 957
IF(KYEAR.GT.MAXYR)GOTO 957
998 CONTINUE
CALL M5TFSH(POPNEW,KYEAR,LAITYR)
997 CONTINUE
CALL STRCT(FRSTYR,LAITYR)
C
CALCULATE PERCENTAGE EGGS LOST BEFORE HATCHING
SUP=C.0
DD 990 I=1,365
C
990 SUM = SUM + EGGCKR(I)
C
PERCENT=SUM/EGGS
WRITE(6,100)PERCENT
995 FORMAT(' THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS ',E12.4)
C
999 IF(KYEAR.LT.LASTYR)GOTO 170
CALL CATCH(FRSTYR,LAITYR)
CALL POPPL(FRSTYR,LAITYR)
CALL M5PLT(FRSTYR,LAITYR)
WRITE(6,1800)NPTMAX
1800 FORMAT(' ,5X, THE MAXIMUM NUMBER OF PARTICLES ',
* ' IN THE SYSTEM AT ANY ONE TIME WAS ',I5,////)
C
KDUM=3132
CALL COPPAR(1CAY,KDUM,INTELM)
C
DD 1820 I=1,365
IF(PLVTOX(I).EQ.0.0)GOTO 1820
WRITE(6,1810)PLVTOX(I)
1810 FORMAT(' ,5X, DAY SPANNED: ',I6,
* ' ,5X, NUMBER OILED: ',E12.4)
1820 CONTINUE
C
IF(OUTPOP.EQ.0)GOTO 1826
REWIND 15
DD 1825 I=1,18
WRITE(15,1825)POPNEW(I)
1825 CONTINUE
1826 CONTINUE
C
WRITE(6,1830)
1830 FORMAT(40X,///,' *****NORMAL TERMINATION*****')
RETURN
END
C
.....
SUBROUTINE COPPAR(1CAY,KYEAR,INTELM)
C
.....
COMPARES RATES OF REDUCTION IN NUMBERS PER UNIT VOLUME
DUE TO MORTALITY AND DIFFUSION
C
INTEGER ICAT(2),INTELM(10)
REAL SUM1(2)
C
COMMON /LINK/ PLVOLD(365), PLVTOX(365), DILCCN(148),
* X0ILMN,X0ILM,X0ILPM,X0IL4P,
* XOSPIL(151),YOSPIL(151),ROSPIL(151),NSPIL

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REAL LRVSUM(365)
COMMON /EGG/ DESOWN,OIL
LOGICAL DOPPN,OIL
COMMON /TZARR/ ICCN,TEW,IND,INOD,TELP,ITMP
INTEGER*2 ICOD(2,25),I1(19),I2(19),IND(3400),INDI(2,153)
INTEGER*2 TELP(2,25),I1(19),I2(19)
COMMON /RAARR/ PART,ELATN,RSLP,SVEL,PRTOLO,UWNET
REAL*4 PART(17,2019),ELATN(3,153),RSLP(3,251),SVEL(3,153)
REAL*4 PRTOLO(2,2019),UWNET(2,153)
COMMON /L1ARR/ LGNDY,SGNET
LOGICAL*1 SGNDY(3,251),SGNET(2019)
COMMON /TAVAR/ IN,IT,IP,IF,IFA,IFB,IFC,IPOND,INTKA,INTRB,NPLT,
* NRR,NIR,NYB,NYR,NLSTR,JPLT,NMCT
* TELT,ISTOP,ISTEC,ANN,NE,NP,NT,NV,NMAX,NENAX,NPHAX
C
COMMON /L1VAR/ TE
COMMON /RAVAR/ UP,VP,UPA,VPA,UPD,VPD,UV,ZERO,XMIN,YMIN,
* XMEAN,YMEAN,XMAX,YMAX,DXV,DYV,CNCL,UNCL,VNET,
* ARX,ARY,ARN,ARN,ARA,AWRT,PLT,OWRT,UPLT,
* DT,TMF,TIMEV,RNA,RNB,MGT,SFX,SFY,RXF,YOFF
C
COMMON/ARRAYS/ POPNEW(10),POPNI(9),SURVE(10),PCPUL(10),
* FCI(18),PREC(18),PLARVA(365,10),SUMPN,EGGCKR(365)
COMMON /OUTPTS/ POPSI(179),NDISI(18),DIFFI(18),
* YRMAS(179),WICAL(18),EFFI(18),EAPFI(18),
* RLCCHI(79),EFFORT(79),SEL(18),CCATCH(79)
C
CALLED ONCE JUST BEFORE ADVECTION ON DAY IDATE, ONCE JUST AFTER,
ONCE AFTER MORTALITY, AND ONCE AT THE VERY END FOR RESULTS
C
IF(NP.EC.0)RETURN
ICNT=ICN1+1
IF(1CNT.GT.3.AND.KYEAR.NE.3132)RETURN
IF(1CNT.EQ.1)GOTO 100
IF(1CNT.EQ.2)GOTO 105
IF(1CNT.EQ.3)GOTO 100
IF(1CNT.EQ.4)GOTO 105
IF(1CNT.EQ.5)GOTO 100
IF(1CNT.EQ.6)GOTO 105
IF(1CNT.EQ.7)GOTO 100
IF(1CNT.EQ.8)GOTO 105
IF(1CNT.EQ.9)GOTO 100
IF(1CNT.EQ.10)GOTO 105
100 DO 105 I=1,10
DO 105 J=1,3
105 SUP(I,J)=0.0
IDAY=IDAY
KYEAR=KYEAR
C
DO 140 I=1,NP
COMMON /CCUMT/ CCUMT TODAY'S
IF(PART(I,1).EQ.1CAY)GOTO 140
DO 110 J=1,10
IF(1TELP(I).EQ.1INTELM(J))GOTO 120
110 CONTINUE
DO 120 I=1,10
DO 120 J=1,10
120 SUP(I,J)=SUM(I,J) + PART(I,1)
140 CONTINUE
RETURN
C
NOW AFTER ADVECTION; DO IT AGAIN
DO 240 I=1,NP
IF(PART(I,1).EQ.1CAY)GOTO 240
DO 210 J=1,10
IF(1TELP(I).EQ.1INTELM(J))GOTO 220
210 CONTINUE
DO 220 I=1,10
DO 220 J=1,10
220 SUP(I,J)=SUM(I,J,2) + PART(I,1)
240 CONTINUE
RETURN
C
AND HERE AFTER MORTALITIES
DO 340 I=1,NP
IF(PART(I,1).EQ.1DAY)GOTO 340
DO 310 J=1,10
IF(1TELP(I).EQ.1INTELM(J))GOTO 320
310 CONTINUE
DO 320 I=1,10
DO 320 J=1,10
320 SUP(I,J)=SUM(I,J,3) + PART(I,1)
340 CONTINUE
RETURN
C
AND HERE AT THE END TO CALCULATE AND OUTPUT
400 WRITE(6,800)IDAY,KYEAR
800 FORMAT(' ***** THESE ARE THE LOSS RATES IN 10 ELEMENTS ',
* ' DUE TO TRANSPORT AND MORTALITY ON DAY ',I4, ' YEAR ',I5)
WRITE(6,810)
810 FORMAT(' ,5X, ELEMENT ',5X, ' INITIAL NUMBER ',5X,
* ' PERCENT TRANSPORTED ',5X, ' PERCENT DIED ',5X, ' RATIO ')
C
NOW CALCULATE
DO 440 I=1,10.
TRANS=0.0
IMCR=0.0
RATIO=0.0
IF(SUM(I,1).EQ.0.0)GOTO 440
TRANS=SUM(I,1)-SUM(I,2)
IMCR=SUM(I,1)-SUM(I,3)
TRANS=1-TRANS/SUM(I,1)*100.0
RATIO=TRANS/IMCR
440 WRITE(6,820)INTELM(I),SUM(I,1),TRANS,IMCR,RATIO

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```

B20 FCNMT117,5X,E13.4,5X,F13.5,10X,F13.5,5X,F10.4)
RETURN
END
C
C.....
C SUBROUTINE BYPASSING TIME EPIC,EM1,EM2,EM3,EM4,EM5,EM6,
YEAR,D12,DELTA,T,EM,F,RYEAR,ICROP,CADPRT)
C.....
C INTEGER SPILVR,SPILDA,SPILTP
COMMON /SPILL/ SPILVR,SPILCA,MRYDAY,MRYR,IADV,IDLST,SPILTP,
SPILAG
C COMMON /LOGIC/ DOSPWN,OIL
COMMON /ARRAYS/ PCPNEM(18),PCPN(18),SURV(18),POPOLD(18),
SUMPN,EGGCH(365)
C COMMON /OUTPTS/ POPS(2170),LTDIST(18),DIFF(18),
YPM(5170),WTCALC(18),EXPM(18),ENPF(18),
RLCTCH(70),EFIC(119),SEL(18),CLATCH(7)
C COMMON /LINK/ PLVOLD(365),PLVOT(365),DILCON(140),
ROILN,ROILM,VOILNH,DILM,
ROSPIL(18),YCSPL(51),ROSPIL(51),MSPIL
C.....
C THERE'S WHERE TO MAKE QUICK WORK OF A YEAR'S TIME WITHUJT
C DAILY TIMESTEPS, WHICH ARE UNNECESSARY IF PHYSICAL DISTRIBUTIONS
C ARE NOT OF INTEREST.
C 60 MONTHS OF SPANNING: 18 DAYS AS EGGS, 10 DAYS AS VOLKSA CLARVAL,
C 4 DAYS TO ADAPT, 100 DAYS AS FREEFEEDERS
C ANDINGST THE OTHER PLANKTON, AND 235 DAYS DEMERSAL
C
EXPDI=ENPF(2170)*0.365*0.1
EXPDI2=ENPF(2170)*0.365*0.1
DUM1=(EM10/EM11)*EXPDI-1.0
DUM2=(EM13/EM21)*EXPDI2-1.0
DO 227 I=1,365
TIME=I
CALL SPNTIME(TIME,DELTA,DISTRB)
PLARVA(1:1)=PCPN(11)*DISTRB
DO 4 I=1,18
PLARVA(1:1)=PLARVA(1:1)/(DUM1*PLARVA(1:1)+EXPDI)
PLARVA(1:1)=PLARVA(1:1)/(DUM2*PLARVA(1:1)+EXPDI)
227 CONTINUE
SUMPN=0.0
DO 219 I=2,10
SUMPN=SUMPN+(IPRED(11)*PCPNEM(11))
F=EM * F
DUMNY=235.0/D12
DO 220 I=1,DUMNY
220 CALL BTHRT(EM14,EM15,EM16,10AY,DT2)
DO 229 I=1,365
229 RCTCH=ACTCH * PLARVA(1:1)
IF ICROP.EQ.1.AND.RYEAR.EQ.SPILVIRACTCH-RCTCH*CADPRT
C NOW CYCLE THE ACCLTS
C
DO 221 I=1,17
221 J=EMEM(18)*PCPN(1)
POPNEW(18)=PCPN(17)+PCPN(18)
POPNEW(21)=RCTCH
C
RETURN
END
C.....
C SUBROUTINE MODDIL(SPILVR,MULTI,DILSTP,IRWIND)
C WHENEVER MULTI GT 1 AND RYEAR GT SPILVR, CALL THIS SR TO SEE
C WHAT THE NEW VALUE FOR SPILVR IS. SPILDA COULD BE RANDOMLY
C VARYING BUT SHOULD LEAVE IT STEADY FOR MOD.
COMMON /LOGIC/ DOSPWN,OIL
LOGICAL OIL,DOSPWN
INTEGER IC(17),DILSTP,SPILVR
C
ICAT=IC(1)
IF IC(1).MULTI*RETURN
SPILVR=SPILVR * DILSTP
OIL=.TRUE.
IF IRWIND.EQ.1,IRWIND=3
CALL INTI
RETURN
END
C.....
C SUBROUTINE WEIGHT
C.....
C THE CONVERSION FROM AGE TO WEIGHT IS
C ACCOMPLISHED VIA GIFFORD AND PENTILLA (1976)
C AND GIFFORD AND SCHROEDER(1955)
C THE FORMER IS A VON BERTALANFY FIT
C THE LATTER IS A LOGISTIC GROWTH CURVE
C FITTED BY LEAST SQUARES
C
USE PENTILLA AND GIFFORD TO CAL LENGTH AT AGE

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C THEN USE THOSE LENGTHS TO CAL CORRESPONDING WEIGHTS
C FOR SUCCESSIVE AGE CLASSES, AND MULTIPLY BY THE
C INPUT DENSITY TO GET
C.....
C DIMENSION ALICAL(18)
COMMON /OUTPTS/ POPS(2170), LTDIST(18),DIFF(18),
YPM(5170),WTCALC(18),EXPM(18),ENPF(18),
RLCTCH(70),EFFORT(70),SEL(18),CCATCH(70)
C
WRITE(6,15)
DO 30 I=1,18
1=F*O(1:1)
Z=1-O.L2*(1+O.614)
ALICAL(1)=148.1*(1-O-EXP(Z))
WTCALC(1)=30.35/11.0 * (301.0*EXP(X11))
JJ=1-1
WRITE(6,16)JJ,WTCALC(1),ALICAL(1)
15 FORMAT(12,'AGE',7X,'CALCULATED WEIGHT (KG)',7X,
8,'CALCULATED LENGTH (CM)')
16 FORMAT(12,'13,10X,F15.3,11X,F15.3)
20 CONTINUE
30 CONTINUE
RETURN
END
C.....
C SUBROUTINE AVGFCE(EGGS)
C B AND S (1973) REPORT AN AVG OF 1 MILLION
C AND A MAX OF 9 MILLION
C COMMON/ARRAYS/ POPNEW(18),PCPN(18),SURV(18),POPOLD(18),
FEC(18),PRED(18),PLARVA(365,10),SUMPN,EGGCH(365)
C
WRITE(6,5)
5 FORMAT(1,'EGGS
2 FORMAT(1,'THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS ',E10.4)
C
C CALCULATE THE AVG PER FEMALE
C
SPAWN=0.0
DO 4 I=1,18
4 SPAWN=SPAWN + (POPNI(1)/2.0)
AVERAG=EGGS/SPAWN
WRITE(6,5)
5 FORMAT(1,')
6 WRITE(6,6)AVERAG
6 FORMAT(1,'THE AVERAGE NUMBER OF EGGS PER FEMALE IS ',E10.3)
WRITE(6,5)
RETURN
END
C.....
C SUBROUTINE SPNTIME(TIME,DELTA,DISTRB)
C.....
C CALCULATES THE SPANNING DISTRIBUTION IN TIME
COMMON /LOGIC/ DOSPWN,OIL
LOGICAL DOSPWN,OIL
C
DOSPN=TRUE
IF 10.0.LT.TIME.AND.TIME.LE.30.0,DISTRB=0.05*(DELTA/30.0)
IF 30.0.LT.TIME.AND.TIME.LE.60.0,DISTRB=0.05*(DELTA/30.0)
IF 60.0.LT.TIME.AND.TIME.LE.90.0,DISTRB=0.4*(DELTA/30.0)
IF 90.0.LT.TIME.AND.TIME.LE.120.0,DISTRB=0.10*(DELTA/30.0)
IF 120.0.LT.TIME.AND.TIME.LE.300.0,DISTRB=0.0
IF 300.0.LT.TIME.AND.TIME.LE.330.0,DISTRB=0.3*(DELTA/30.0)
IF 330.0.LT.TIME AND TIME.DISTRB=0.10*(DELTA/30.0)
IF DISTRB.EQ.0.0,DOSPWN=.FALSE.
RETURN
END
C.....
C SUBROUTINE DEVELOP(DAY,RECRUT)
C.....
C COMMON/ARRAYS/ POPNEW(18),PCPN(18),SURV(18),POPOLD(18),
FEC(18),PRED(18),PLARVA(365,10),SUMPN,EGGCH(365)
C THE FIRST YEAR THROUGH
C PLARVA(1:1) : THE HATCH ESTABLISH VALUES FOR
C PLARVA(1:6) : THE HATCH YIELD TIME
C PLARVA(7:7) : THE PLANKTONI (FREEFEEDING ADAPTION TIME
C PLARVA(18) : THE PLANKTONI CTIME
C INTERP. R. EQUIN/D
IF ICOUNT.GT.364,GO TO 2
ICOUNT=ICOUNT+1
DO 3 I=1,53
3 TAVE=TIME(DAY,DEGC)
CALL TEMP(DAY,DEGC)
SUM=FLQ(1)
SUM=SUM+DEGC
TAVE=SUM/ANUM
CALL MATCHTAVE(DAYS)
IF ANUM.GE.DAYS) PLARVA(DAY,9)=DAYS
IF ANUM.GE.DAYS) GO TO 1
CONTINUE
3
C THAT WAS MATCHTIME
C VOLTIME NEXT

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1000 ICNT=1
DO 14 I=1,ICNT
  WRITE(10,806)ICMAX
  FORMAT(17,7) 'THE MAXIMUM SUBSURFACE CONCENTRATION IS *
  F10.2,7) PARTS PER BILLION ABOVE BACKGROUND LEVELS.',7)
  WRITE(10,807)NUMELM,DI,DT
  FORMAT(17,7) 'THERE ARE * I5,7) ELEMENTS OUT THERE, WITH GRID *
  SPACING OF * 2E10.3,7) MAP UNITS.'
  CNOW WRITE TO DATA SET 4 TODAY'S LARVAL AND OIL DISTRIBUTIONS
  DO 9 I=1,12
    IF (ICDAY.EQ.IDAYZ(1)) GO TO 11
  CONTINUE
  RETURN
11 CONTINUE
  IF (ICNT.GT.0) GO TO 10
  ICNT=1
  WRITE(10,810)SPILYR,SPILDA,IAOV,IDAIST,SPLTYP,THRSLD
  WRITE(10,811)ICDAY,KOILMX,KOILRX,VOILMX,VOILRN,MP,DX,DV,NJMELM
  WRITE(10,812)NSPIL
  DO 10 I=1,NSPIL
    WRITE(10,813)XOSPIL(I),YCSPIL(I),ROSPIL(I)
  CONTINUE
  DO 35 I=1,NUMELM
    WRITE(10,814)CONC(I),JKI,JK=1,3)
    TO 20 I=1,12
    IMDUM=PART(I,1)
    IF (IMDUM.LT.1) OR (IMDUM.GT.36) GO TO 41
    IMDUM=15 * I * PLARVAL(IMDUM,2)
    GO TO 42
  41 IMDUM=5
  42 CONTINUE
  WRITE(10,815)PART(I,1),J=1,3) IMDUM, PART(I,1)
  CNOW VLOC, 8) DAY SPANNED, ELEMENT NUMBER
  CONTINUE
  RETURN
900 ICNT=1
1000 ICNT=1
KOILRN=100.0
VOILRN=100.0
VOILMX=100.0
VOILRX=100.0
VLOC=.FALSE.
NSPIL=0
WRITE(10,802)SPILCA,ICDAY
802 FORMAT(17,7) 'THE OIL SPILL BEGAN ON DAY * I5,7) //
  AND ITS DIRECT EFFECTS ON THE FISHERY ENDED ON DAY * I5,7) //
  RETURN
END
*****
SUBROUTINE DSCWRT(ICDAY)
*****
COMMON /LINK/ PLVLOC(365), PLVTR(365), OILCON(148),
  KOILRN, VOILRN, VOILMX, VOILRX,
  ROSPIL(151), VOSPIL(151), ROSPIL(151), NSPIL
COMMON /LOGIC/ DCSPPN, OIL
LOGICAL DCSPPN, OIL
COMMON /I2ARR/ ICEN, IEN, IND, INOD, IELP, ITMP
INTEGER 2 ICEN(2,251), IEN(3,251), INDI(3400), INODI(2,153)
INTEGER 2 IELP(2,191), ITMP(2,2019)
COMMON /R4ARR/ PART, CAIN, RSLP, SVEL, PRTOLO, UVNET
REAL 4 PART(7,2019), DATN(3,153), RSLP(3,251), SVEL(3,153)
COMMON /I1PRP/ SGNDY, SGNPT
LOGICAL 1 SGNDY(3,251), SGNPT(2019), TF, SGNX
COMMON /I4VAR/ IN, IT, IP, IE, IF, IRA, IRB, IOP, IPCND, INTKA, INTRK, NPLT,
  NWPL, INTKI, NVR, NVRC, ISTR, JPL, NRCT
COMMON /I1VAR/ UP, VP, UPA, VPA, UPD, VPD, UV, ZERU, XMIN, YMIN,
  XMAX, YMAX, XPA, YPA, XPD, YPD, CONL, UNET, VNET,
  AR, ARY, ARX, ARN, ARB, ARW, TRWT, IPLT, DTWRT, DTPLT,
  DT, TIME, TIMEV, PNA, PNR, HGT, SFX, SFY, XOFF, YOFF
COMMON /ARRAYS/ POPN(18), POPN(18), SURV(18), POPULO(18),
  FFC(18), PRE(18), PLARVAL(365), SUNN, EGGCN(365)
COMMON /OUTPTS/ POPS(279), A(10), DIST(18), DIFF(18),
  VMASS(79), WTCALC(18), EXFM(18), EAPF(18),
  RLC(179), EFC(179), SEL(18), CLAF(18)
COMMON /BLWOUT/ CONC(398,3), NUMELM, THRSLD, DX, DY, IDAYZ(12)
INTEGER INTRE/0
IF (INP.EQ.0) RETURN
IF (INTRO.GT.0) GO TO 11
INTRE=1
WRITE(10,881)ICAYZ(1),I=1,12)
881 FORMAT(17,7) I4,1X)
CONTINUE
DO 12 I=1,12
  IF (ICAYZ(I).EQ.ICLAY) GO TO 10

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12 CONTINUE
10 RETURN
10 CONTINUE
WRITE(10,798)IDAY
800 FORMAT(17,7) 'HERE IS THE DISTRIBUTION FOR DAY * I4,1X)
797 FORMAT(17,7) 'DAY * I8,7) LARVAL DISTRIBUTION WRITTEN TO *
  DISC * I3,7)
799 FORMAT(17,7) 'DAY * I12,7) VLOC, VLOC,
  130 NUMBER * I4C,7) DAY SPANNED * 2X,7) STAGE * 2X,7) ELEMENT *
  WRITE(10,800)IDAY (PART(I,1),J=1,3), PART(I,1),
  800 PLARVAL(PART(I,1),J=1,3), IELP(I)
800 FORMAT(2X,14,2) I4,2) I4,2) I4,2) I4,2) I4,2) I4,2) I4,2) I4,2) I4,2)
90 CONTINUE
RETURN
END
SUBROUTINE ADVDF(ICDAY,NPTMAX,IOFF)
COMMON /I2ARR/ ICEN, IEN, IND, INOD, IELP, ITMP
INTEGER 2 ICEN(2,251), IEN(3,251), INDI(3400), INODI(2,153)
INTEGER 2 IELP(2,191), ITMP(2,2019)
INTEGER INTRE/0
COMMON /R4ARR/ PART, CAIN, RSLP, SVEL, PRTOLO, UVNET
REAL 4 PART(7,2019), DATN(3,153), RSLP(3,251), SVEL(3,153)
COMMON /I1PRP/ SGNDY, SGNPT
LOGICAL 1 SGNDY(3,251), SGNPT(2019), TF, SGNX
COMMON /I4VAR/ IN, IT, IP, IE, IF, IRA, IRB, IOP, IPCND, INTKA, INTRK, NPLT,
  NWPL, INTKI, NVR, NVRC, ISTR, JPL, NRCT
COMMON /I1VAR/ UP, VP, UPA, VPA, UPD, VPD, UV, ZERU, XMIN, YMIN,
  XMAX, YMAX, XPA, YPA, XPD, YPD, CONL, UNET, VNET,
  AR, ARY, ARX, ARN, ARB, ARW, TRWT, IPLT, DTWRT, DTPLT,
  DT, TIME, TIMEV, PNA, PNR, HGT, SFX, SFY, XOFF, YOFF
IF (INTRO.GT.0) GO TO 100
CALL FEREAD
CALL VAREAD
CALL YAREAD
CALL XCHECK
100 CONTINUE
INTRE=INTRO+1
WRITE(10,200)INTRE
200 FORMAT(17,7) 'THIS IS ENTRY NUMBER *
  TO SUBROUTINE ADVDF *
  IF (INP.GT.0) MAX(NPTMAX,NP)
  IF (INP.EQ.0) GO TO 300
  NP=0
  NOUT=0
CALL SPNPLC(ICDAY)
IF (INP.GT.0) MAX(NPTMAX,NP)
CONTINUE
CALL MCVE(INTRO,ICDAY)
IF (INP.GT.0) MAX(NPTMAX,NP)
CALL BEAD(IOFF)
CALL CCMRPS
CALL ESCWRT(ICDAY)
RETURN
END
SUBROUTINE MCVE(INTRE,ICDAY)
SUBROUTINE MCVE(INTRE,ICDAY) IS THE MAIN SUBROUTINE WHICH ADVECTS
AND DIFFUSES THE PARTICLES.
COMMON /LOGIC/ DCSPPN, OIL
COMMON /I2ARR/ ICEN, IEN, IND, INOD, IELP, ITMP
INTEGER 2 ICEN(2,251), IEN(3,251), INDI(3400), INODI(2,153)
INTEGER 2 IELP(2,191), ITMP(2,2019)
COMMON /R4ARR/ PART, CAIN, RSLP, SVEL, PRTOLO, UVNET
REAL 4 PART(7,2019), DATN(3,153), RSLP(3,251), SVEL(3,153)
COMMON /I1PRP/ SGNDY, SGNPT
LOGICAL 1 SGNDY(3,251), SGNPT(2019), TF, SGNX
COMMON /I4VAR/ IN, IT, IP, IE, IF, IRA, IRB, IOP, IPCND, INTKA, INTRK, NPLT,
  NWPL, INTKI, NVR, NVRC, ISTR, JPL, NRCT
COMMON /I1VAR/ UP, VP, UPA, VPA, UPD, VPD, UV, ZERU, XMIN, YMIN,
  XMAX, YMAX, XPA, YPA, XPD, YPD, CONL, UNET, VNET,
  AR, ARY, ARX, ARN, ARB, ARW, TRWT, IPLT, DTWRT, DTPLT,
  DT, TIME, TIMEV, PNA, PNR, HGT, SFX, SFY, XOFF, YOFF
IF (INTRO.GT.1) GO TO 5
NP=0
NOUT=0
DEPWIN=12.
DEPRN=12.
DEPSLP=1.7*(DEPPAX-DEPRN)
UPD=0.0
VPD=0.0
5 CONTINUE
IF (INP.EQ.0) RETURN
TIME LOOP
DO 1000 IT=1,NIT
  CALL VELINI(ICAY)
ADD VEL LARVAE
IF (DOSPWN) CALL SPNPLC(ICDAY)
IF (INP.EQ.0) GO TO 3000
DO 2000 I=1,NP
  IF (IND(SGNPT(I))) GO TO 2000

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NEMAX = 25
NPMAX = 1010
DO 10 I=1,NPMAX
  IELP(I) = 1
  CONTINUE
  DO 11 J=1,TRUE
    PART(I,J) = 0.0
    DO 12 J=1,2
      TIME(J,I) = C
      PRTOLO(J,I) = 0.0
    CONTINUE
  10 CONTINUE
  IF (INTNO.GT.1) GO TO 45
  DO 19 I=1,12
    IDATZ(I) = 0.0
    DO 20 I=1,NEMAX
      DO 22 J=1,2
        ICCAT(J) = 0
      CONTINUE
    27 CONTINUE
    DO 24 J=1,3
      IEN(J,I) = 0
      RSLPJ(J,I) = 0.0
      SGNDY(J,I) = .TRUE.
    CONTINUE
    20 CONTINUE
    DO 26 J=1,3400
      IND(J) = 0
    CONTINUE
    26 CONTINUE
    DO 30 I=1,NMAX
      DO 32 J=1,3
        UVNET(J,I) = 0.0
        IND(J,I) = C
      CONTINUE
    32 CONTINUE
    DO 34 J=1,3
      SVEL(J,I) = 0.0
      EATN(J,I) = 0.0
    CONTINUE
    34 CONTINUE
    30 CONTINUE
    IRR = 50*15
    RMA = 2.0*32.0
    SGNK = .TRUE.
    TIME = 0
    CENL = 1
    DO 40 I=1,365
      PLVOT(I) = C.0
    CONTINUE
    40 CONTINUE
    ***** THESE ARE THE STORAGE LOCATIONS FOR THE CENTROIDS AND RADII OF THE
    ***** SPILLS AND THE EXTREMES OF THE SUBSURFACE DISTRIBUTION.
    NSPIL(I) = C.0
    NSPILM(I) = 100.0
    NSPILX(I) = 100.0
    NSPILY(I) = 100.0
    NSPILZ(I) = 100.0
    NSPILW(I) = 100.0
    NSPILV(I) = 0
    DO 60 I=1,300
      CONCT(I) = 0.0
    60 CONTINUE
    DR = 0.0
    RETURN
  END
SUBROUTINE FEREAD
C
C SUBROUTINE FEREAD READS THE FINITE ELEMENT DATA
COMMON /I2ARR/ ICCA, IEN, INC, INOD, IELP, IIMP
INTEGER*2 ICON(2,251), IEN(3,251), IND(3400), INOD(2,153)
INTEGER*2 IELP(2019), IIMP(2,2019)
COMMON /R4ARR/ PART, EATN, RSLP, SVEL, PRTOLO, UVNET
REAL*4 PART(7,2019), EATN(3,153), RSLP(3,251), SVEL(3,153)
REAL*4 PRTOLO(2,2019), UVNET(2,153)
LOGICAL*1 SGNDY(3,251), SGMPT(2019), IF, SGNK
COMMON /I4VAR/ IN, IT, IP, IF, IRA, IRB, IRD, IPCND, INTKA, INTKB, NPLT,
NVRT, INTRT, KVP, NVRC, ISFRT, JPLT, NRCT,
IFLCT, ISTOP, ISEED, AN, NE, NP, RT, NV, NMAX, NEMAX, NPMAX
COMMON /L1VAR/ TF
COMMON /R4VAR/ UP, VP, UPA, VPA, UPD, VPD, UV, ZER0, XMIN, YMIN,
XMAX, YMAX, XAN, YAN, XAR, YAR, DXV, DTV, CONL, UVNET, VNET,
ARR, ARY, ARZ, ARH, ARS, ARW, ARX, ARY, ARZ, ARH, ARS, ARW, ARX, ARY, ARZ,
DT, TIME, TIMEV, RNA, RNB, HGT, SFX, SFY, RKF, YOFF
WRITE(6,603)
NN = NUMBER OF NODS
NE = NUMBER OF ELEMENTS
READ(10,100) NN, NE
CONTINUE
7 WRITE(6,600) NN, NE
DPSET = 4.0*COS(39.0*3.14159/180.0)
DO 10 I=1, NN
  INOD(I,1) = NOD NUMBER
  DATN(I,1,3,1) = XLLC, YLLC, DEPTH OF NOD I
  INOD(I,2) = NOD TYPE
  READ(11,101) INOD(I,1), YLAT, XLONG
  EATN(I,1) = 100.0
  INOD(I,2) = 0
  DATN(I,1) = CB.0 - RLCNG

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EATN(2,1) = YLAT - 95.0
EATN(1,1) = 3.14159/180.0
DATN(1,1) = EATN(1,1) * CFFSET
DATN(2,1) = DATN(1,1) * CCONL
DATN(3,1) = DATN(1,1) / CCONL
EATN(2,1) = DATN(2,1) / CCONL
10 CONTINUE
XMIN = -1.E20
YMIN = -1.E20
XMAX = -1.E20
YMAX = -1.E20
DO 20 I=1, NE
  IEN(I,1,3,1) = NODS FOR ELEMENT I
  READ(1,102) IRDUM, IEN(I,1,1,3)
  DO 30 I=1,3
    I1 = IEN(I,1)
    XMIN = AMIN(XMIN, DATN(I,1,1))
    YMIN = AMIN(YMIN, DATN(I,2,1))
    XMAX = AMAX(XMAX, DATN(I,1,1))
    YMAX = AMAX(YMAX, DATN(I,2,1))
  30 CONTINUE
  20 CONTINUE
  XMIN = XMIN * CCONL
  XMAX = XMAX * CCONL
  YMIN = YMIN * CCONL
  YMAX = YMAX * CCONL
  WRITE(6,606) XMIN, YMIN, XMAX, YMAX
  RETURN
C
C FORMATS
100 FORMAT(2I5)
101 FORMAT(5,4X,F6.3,4X,F6.3)
102 FORMAT(2H,4(13,3))
600 FORMAT(10,'NUMBER OF NODS =',I5,T40,
* 'NUMBER OF TRIANGULAR ELEMENTS =',I5//)
601 FORMAT(17H,15,3F15.3,110)
602 FORMAT(10,'SUPERICAL PARTICLE TRAJECTORY PROGRAM',//
* 15,'FINITE ELEMENT DATA://')
603 FORMAT(1120,'NODE',T3L,'XLLC',T46,'YLLC',T62,'DEPTH',
* 175,'')
605 FORMAT(1721,'ELEMENT',T35,'NODE A',T45,'NODE B',
* T55,'NODE C',T7)
606 FORMAT(17110,'FIELD SIZE',T30,'XMIN =',E10.4,T50,
* 'YMIN =',E10.4,T70,'XMAX =',E10.4,T90,
* 'YMAX =',E10.4)
END
*****
***** SUBROUTINE VELIN(NDAY)
*****
SUBROUTINE VELIN READS THE VELOCITY DATA
COMMON /I2ARR/ ICON, IEN, INOD, IELP, IIMP
INTEGER*2 ICON(2,251), IEN(3,251), IND(3400), INOD(2,153)
INTEGER*2 IELP(2019), IIMP(2,2019)
COMMON /R4ARR/ PART, EATN, RSLP, SVEL, PRTOLO, UVNET
REAL*4 PART(7,2019), EATN(3,153), RSLP(3,251), SVEL(3,153)
REAL*4 PRTOLO(2,2019), UVNET(2,153)
COMMON /L1ARR/ SGNDY, SGMPT
LOGICAL*1 SGNDY(3,251), SGMPT(2019), TF, SGNK
COMMON /I4VAR/ IN, IT, IP, IF, IRA, IRB, IRD, IPCND, INTKA, INTKB, NPLT,
NVRT, INTRT, KVP, NVRC, ISFRT, JPLT, NRCT,
IFLCT, ISTOP, ISEED, AN, NE, NP, RT, NV, NMAX, NEMAX, NPMAX
COMMON /L1VAR/ TF
COMMON /R4VAR/ UP, VP, UPA, VPA, UPD, VPD, UV, ZER0, XMIN, YMIN,
XMAX, YMAX, XAN, YAN, XAR, YAR, DXV, DTV, CONL, UVNET, VNET,
ARR, ARY, ARZ, ARH, ARS, ARW, ARX, ARY, ARZ, ARH, ARS, ARW, ARX,
DT, TIME, TIMEV, RNA, RNB, HGT, SFX, SFY, RKF, YOFF
C
C WIND CURRENT FOR TODAY
800 READ(14,800,END=101) DAYNO, U, V, WIND
FORMAT(14,2F8.5)
IF (ICAV, NE, IDAYNO) GO TO 5
GO TO 70
10 REWIND 14
GO TO 5
C
C BUNPLC - NET DRIFT DATA
20 CONTINUE
DO 40 I=1, NN
  READ(13,801) ICAYCK, NODNUM, SVEL(2,1), SVEL(3,1)
  IF (ICAY, NE, ICAYCK, OP, I, NE, NODNUM) GO TO 30
  SVEL(2,1) = SVEL(2,1) * UWIND
  SVEL(3,1) = SVEL(3,1) * VWIND
  RETURN
40 REWIND 13
GO TO 20
END
SUBROUTINE VAREAD
C
C SUBROUTINE VAREAD READS THE PARAMETER DATA, THE INITIAL
PARTICLE DATA, AND THE NET DRIFT DATA
COMMON /I2ARR/ ICON, IEN, INOD, IELP, IIMP
INTEGER*2 ICON(2,251), IEN(3,251), IND(3400), INOD(2,153)
INTEGER*2 IELP(2019), IIMP(2,2019)
COMMON /R4ARR/ PART, EATN, RSLP, SVEL, PRTOLO, UVNET
REAL*4 PART(7,2019), EATN(3,153), RSLP(3,251), SVEL(3,153)
REAL*4 PRTOLO(2,2019), UVNET(2,153)
COMMON /L1ARR/ SGNDY, SGMPT

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SUBROUTINE GRAFIX,Y,RR,I)
RETURN
SUBROUTINE PLOTIX,Y,I)
RETURN
SUBROUTINE NUMPLTX,Y,T,H,F,I)
RETURN
SUBROUTINE PLTLNIX,Y,XX,VY)
RETURN
SUBROUTINE CHARIX,Y,VY,CAT,I)
RETURN
SUBROUTINE RESET
RETURN
SUBROUTINE DIMENIX,Y,I,Z)
RETURN
SUBROUTINE ARISIX,Y,NAM,I,M,J,K,I)
RETURN
SUBROUTINE VECTORIX,Y,NUM,INC,ICP,I)
RETURN
SUBROUTINE SCALFIX,Y,N)
RETURN
SUBROUTINE OFFSTIX,Y,I)
RETURN
SUBROUTINE DOTLNIX,Y,Z,M,L)
RETURN
SUBROUTINE MATHIX,Y,Z,T,I)
RETURN
SUBROUTINE CATEIX,Y,Z)
RETURN
SUBROUTINE TIMEIX,Y,Z)
RETURN
END
SUBROUTINE COMPRS
COMMON /LOGIC/ POPNHN,OIL
COMMON /ZARR/ I,CCN,IEI,IND,IMOD,IELP,IIMP
INTEGER*2 ICONI2,Z21,IENI3,Z31,INDI3400I,IMODI2,153I
COMMON /RARR/ PART,CATN,RSLP,SVEL,PRTOLO,UVMET
REAL*4 PARTI1,Z20I9,CATN1,1,3I,RSLP13,Z21I1,SVEL13,153I
COMMON /LARR/ SGNDY,SGNPT
LOGICAL*1 SGNDY13,Z21I1,SGNPT120I9,TF,SGNK
COMMON /IIVAR/ IN,I1,I2,IF,IFR,IRR,IRP,IPOND,INTKA,INTKB,NPLT,
NMRT,INTRT,NVR,NVRC,ISTR,JPLT,NCLT
* CCMHON /IIVAR/ I1,I2,I3,I4,I5,I6,I7,I8,I9,I10,I11,I12,I13,I14,I15,
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I2091,I2092,I2093,I2094,I2095,I2096,I2097,I2098,I2099,I2100,I2101,I2102,I2103,I2104,I2105,I2106,I2107,I2108,I2109,I2110,
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I2151,I2152,I2153,I2154,I2155,I2156,I2157,I2158,I2159,I2160,I2161,I2162,I2163,I2164,I2165,I2166,I2167,I2168,I2169,I2170,
I2171,I2172,I2173,I2174,I2175,I2176,I2177,I2178,I2179,I2180,I2181,I2182,I2183,I2184,I2185,I2186,I2187,I2188,I2189,I2190,
I2191,I2192,I2193,I2194,I2195,I2196,I2197,I2198,I2199,I2200,I2201,I2202,I2203,I2204,I2205,I2206,I2207,I2208,I2209,I2210,
I2211,I2212,I2213,I2214,I2215,I2216,I2217,I2218,I2219,I2220,I2221,I2222,I2223,I2224,I2225,I2226,I2227,I2228,I2229,I2230,
I2231,I2232,I2233,I2234,I2235,I2236,I2237,I2238,I2239,I2240,I2241,I2242,I2243,I2244,I2245,I2246,I2247,I2248,I2249,I2250,
I2251,I2252,I2253,I2254,I2255,I2256,I2257,I2258,I2259,I2260,I2261,I2262,I2263,I2264,I2265,I2266,I2267,I2268,I2269,I2270,
I2271,I2272,I2273,I2274,I2275,I2276,I2277,I2278,I2279,I2280,I2281,I2282,I2283,I2284,I2285,I2286,I2287,I2288,I2289,I2290,
I2291,I2292,I2293,I2294,I2295,I2296,I2297,I2298,I2299,I2300,I2301,I2302,I2303,I2304,I2305,I2306,I2307,I2308,I2309,I2310,
I2311,I2312,I2313,I2314,I2315,I2316,I2317,I2318,I2319,I2320,I2321,I2322,I2323,I2324,I2325,I2326,I2327,I2328,I2329,I2330,
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I2411,I2412,I2413,I2414,I2415,I2416,I2417,I2418,I2419,I2420,I2421,I2422,I2423,I2424,I2425,I2426,I2427,I2428,I2429,I2430,
I2431,I2432,I2433,I2434,I2435,I2436,I2437,I2438,I2439,I2440,I2441,I2442,I2443,I2444,I2445,I2446,I2447,I2448,I2449,I2450,
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I2491,I2492,I2493,I2494,I2495,I2496,I2497,I2498,I2499,I2500,I2501,I2502,I2503,I2504,I2505,I2506,I2507,I2508,I2509,I2510,
I2511,I2512,I2513,I2514,I2515,I2516,I2517,I2518,I2519,I2520,I2521,I2522,I2523,I2524,I2525,I2526,I2527,I2528,I2529,I2530,
I2531,I2532,I2533,I2534,I2535,I2536,I2537,I2538,I2539,I2540,I2541,I2542,I2543,I2544,I2545,I2546,I2547,I2548,I2549,I2550,
I2
```



```

1.4 E+05
0.1 E+04
5.4 E+04
7.2 E+04
NEXT COME THE FECUNDITY FACTORS AND SELECTIVITY FACTORS, RESPECTIVELY:
0.0 0.0 0.0 0.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0
0.020 0.341 0.1 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0
AND THEN THE NUMBER OF EGGS PER GRAM NATURE FF=ALF:
2.00E+05
1976 17.4 25.0
1977 20.0 25.0
1978 20.0 24.4
1979 20.0 23.2
1980 20.0 24.4
1981 20.0 25.76
1982 20.0 24.8
1983 20.0 24.4
1984 20.0 24.8
1985 20.0 25.6
1986 20.0 25.2
1987 20.0 24.8
1988 20.0 24.8
1989 20.0 24.32
1990 20.0 24.16
1991 20.0 25.36
1992 20.0 24.4
1993 20.0 25.12
1994 25.2 25.2
1995 20.0 25.16
1996 20.0 25.4
1997 20.0 24.24
1998 20.0 24.88
1999 20.0 25.92
2000 20.0 23.92
2001 20.0 25.76
2002 20.0 23.84
2003 20.0 24.16
2004 20.0 25.28
2005 20.0 26.08
2006 20.0 24.96
2007 20.0 25.28
2008 20.0 24.72
2009 20.0 24.96
2010 24.0 24.88
2011 25.0 25.0
2012 25.0 25.0
2013 24.0 24.4
2014 25.0 24.4
2015 25.0 24.4
2016 25.0 25.74
2017 25.0 24.8
2018 25.0 24.24

```

```

2019 25.0 24.8
2020 25.0 25.6
2021 25.0 25.2
2022 25.0 25.2
2023 25.0 24.16
2024 25.0 24.32
2025 25.0 24.16
2026 25.0 24.4
2027 25.0 26.74
2028 25.0 24.88
2029 25.0 25.92
2030 25.0 23.92
2031 25.0 25.74
2032 25.0 25.84
2033 25.0 24.16
2034 25.0 25.12
2035 25.0 24.08
2036 25.0 24.96
2037 25.0 24.28
2038 25.0 24.72
2039 25.0 24.96
2040 25.0 24.8
2041 25.0 25.0
2042 25.0 25.0
2043 25.0 24.8
2044 25.0 25.2
2045 25.0 24.4
2046 25.0 25.76
2047 25.0 24.8
2048 25.0 24.24
2049 25.0 24.8
2050 25.0 25.6
HERE ARE THE PREDATION MORTALITIES OF OLDER FISH ON THE ZEROTH
0000.00 0003.50 0008.50 0013.00 0019.00 0026.00 0034.00 0043.00
0053.00 0053.00 0053.00 0053.00 0053.00 0053.00 0053.00 0053.00
MGRPS=030
MLOC =67.200, YLOC=41.900PADILS=CC.500
/*
//FF10F001 DD *
0015 0246
01 1.00000 001.C0C00 0 1
10. 2000CC. 0
00.00100 783C&R 1000.
149 0 1C0C.
1 150 151
0.10000 0.1C000 171000. 90000. 0.08000
00000 1.0000C 1.000CC
/*
//FF11F001 DD DSM=URI.LCF1.NODES,DISP=SHR
//FF12F001 DD DUMMY
//FF13F001 DD DSM=URI.LCF1.BUMPUS.CNETEAR,DISP=SHR
//FF14F001 DD DSM=URI.LCF1.WINDCURI,DISP=SHR

```

```

//FF15F001 DD DUMMY
/*
// HERE COME THE CAYS FOR OUTPUT OF LARVAL DISTRIBUTIONS TO UISC
//FF16F001 DD *
0350 030C 0005 0015 0025 0045 0060 0075 0090 0105E120=000GJUUU#
/*

```

V. Sample Output

POSTYR= 1977 LASTYR=2020 ESTYR=1976

THERE WILL BE 1 OILSPILLS SEPARATED BY 4 YEARS EACH.

RATIO OF FEMALES IN THE POPULATION = 0.5000
 ADULT NATURAL MORTALITY = 0.3000
 STARTUP FISHING MORTALITY = 0.2000
 FULL-BLANKET FISHING MORTALITY = 0.3000
 CATCHABILITY COEFFICIENT = 0.0125

DELTA T FOR THE FISHERY MODEL IS 1.0000 DAYS.

THE SHORTCUT TIMESTEP IS 5.0000 DAYS.

MISTDGRAMS WILL BE PRODUCED FOR YEARS 1932 TO 1934.

HERE ARE THE ELEMENTS IN WHICH MORTALITY AND DIFFUSION RATES WILL BE COMPARED ON DAY 365
 00 01 02 101 100 122 123

***** THE CONTROL VARIABLES *****

IS ADVECTION INCLUDED (ISLCON)?	1
IS OFF-THE-BANK MORTALITY INCLUDED (IOFF)?	0
USE 1 BYPASS TIMESTEP AFTER YEAR (YEARLY)?	1981
READ DATASET 3 OR USE A NEW ONE FOR MULTIPLE RUNS (IRNUN)?	1
READ INITIAL POPULATION FROM CARDS (I) OR FILES (II) (INTPOP)?	0
WRITE OUT THE LAST YEAR POPULATION TO FILE (OUTPOP)?	0
FIRST YEAR OF THE RUN (IRSTYR)?	1977
LAST YEAR OF THE RUN (LASTYR)?	2020
STARTUP YEAR (ISTART)?	1976
NUMBER OF OILSPILLS IN THE SERIES (MULT)?	1
NUMBER OF YEARS BETWEEN SPILLS (OILSTP)?	4
YEAR OF THE FIRST SPILL (SPILYR)?	1976
JULIAN DAY OF THE SPILL (SPILCD)?	150
DAY TO BEGIN TRACING DAILY MORTALITY OF EGGS AND LARVAE (TRTDAY)?	350
YEAR IN WHICH THE TRACING BEGINS (OUTRST TO FILE) (TRTYR)?	1981
LAST DAY FOR ADVECTION (LASTD)?	100
ADVECTION WITHOUT OIL (ADCON)?	0
SPLITP = 1 THEN ITS SHORT, =2 THEN A BLOWOUT	2
THE THRESHOLD TOXICITY IN PARTS PER BILLION IS	80.00
IS THIS AN ARTIFICIAL CROPPING RUN? (ICROP)?	0
CROPPING RATE FOR RECRUITS DURING SPILLO (CROPR)?	0.0
ER10 = 0.1500E-03 ER11 = 0.2000E 00 ER12 = 0.2000E 00 ER13 = 0.1000E-19	
ER14 = 0.2000E 00 ER15 = 0.1000E-19 ER16 = 0.1500E-19	

AGE GROUP	INITIAL NUMBERS	CALCULATED LENGTH (CM)	LENGTH (CM)	CALCULATED LENGTH (CM)
0	0.0	0.0	0.0	0.0
1	0.10E 09	0.368	20.100	0.368
2	0.87E 07	0.314	27.101	0.314
3	0.51E 07	0.155	32.130	0.155
4	0.30E 07	0.033	61.180	0.033
5	0.23E 07	0.024	71.012	0.024
6	0.17E 07	0.024	81.140	0.024
7	0.10E 07	0.012	88.110	0.012
8	0.07E 06	0.009	90.110	0.009
9	0.04E 06	0.006	101.300	0.006
10	0.03E 06	0.004	106.072	0.004
11	0.02E 06	0.004	111.070	0.004
12	0.01E 06	0.003	115.111	0.003
13	0.01E 06	0.003	115.106	0.003
14	0.01E 06	0.003	127.505	0.003
15	0.01E 06	0.003	131.070	0.003
16	0.01E 06	0.003	131.070	0.003
17	0.01E 06	0.003	132.113	0.003
18	0.01E 06	0.003	132.113	0.003

AGE	SECURITY
0	0.0
1	0.0
2	0.0
3	0.0
4	0.0
5	0.0
6	0.0
7	0.0
8	0.0
9	0.0
10	0.0
11	0.0
12	0.0
13	0.0
14	0.0
15	0.0
16	0.0
17	0.0
18	0.0

YEAR	CATCH (TONS)	EFFORT (1000S)	EFFICIENT (HOURS)
1976	1.000	1.000	1.000
1977	1.000	1.000	1.000
1978	1.000	1.000	1.000
1979	1.000	1.000	1.000
1980	1.000	1.000	1.000
1981	1.000	1.000	1.000
1982	1.000	1.000	1.000
1983	1.000	1.000	1.000
1984	1.000	1.000	1.000
1985	1.000	1.000	1.000
1986	1.000	1.000	1.000
1987	1.000	1.000	1.000
1988	1.000	1.000	1.000
1989	1.000	1.000	1.000
1990	1.000	1.000	1.000
1991	1.000	1.000	1.000
1992	1.000	1.000	1.000
1993	1.000	1.000	1.000
1994	1.000	1.000	1.000
1995	1.000	1.000	1.000
1996	1.000	1.000	1.000
1997	1.000	1.000	1.000
1998	1.000	1.000	1.000
1999	1.000	1.000	1.000
2000	1.000	1.000	1.000
2001	1.000	1.000	1.000
2002	1.000	1.000	1.000
2003	1.000	1.000	1.000
2004	1.000	1.000	1.000
2005	1.000	1.000	1.000
2006	1.000	1.000	1.000
2007	1.000	1.000	1.000
2008	1.000	1.000	1.000
2009	1.000	1.000	1.000
2010	1.000	1.000	1.000
2011	1.000	1.000	1.000
2012	1.000	1.000	1.000
2013	1.000	1.000	1.000
2014	1.000	1.000	1.000
2015	1.000	1.000	1.000
2016	1.000	1.000	1.000
2017	1.000	1.000	1.000
2018	1.000	1.000	1.000
2019	1.000	1.000	1.000
2020	1.000	1.000	1.000
2021	1.000	1.000	1.000
2022	1.000	1.000	1.000
2023	1.000	1.000	1.000
2024	1.000	1.000	1.000
2025	1.000	1.000	1.000
2026	1.000	1.000	1.000
2027	1.000	1.000	1.000
2028	1.000	1.000	1.000
2029	1.000	1.000	1.000
2030	1.000	1.000	1.000

FOLLOWING ARE THE PRICES OF THE OLDER COD IN THE JUVENILES OF THE YEAR:
 10.00 15.00 20.00 25.00 30.00 35.00 40.00 45.00 50.00 55.00

SILVA = 1074 SPILVA = 330 EACV = 0 ICALST = 100 SPLTP = 2184LD = 0.0002 PARIS PER BILLION

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1077	0.100	0.20
2	0.1788	0.112	0.20
3	0.2599	0.124	0.20
4	0.3410	0.136	0.20
5	0.4221	0.148	0.20
6	0.5032	0.160	0.20
7	0.5843	0.172	0.20
8	0.6654	0.184	0.20
9	0.7465	0.196	0.20
10	0.8276	0.208	0.20
11	0.9087	0.220	0.20
12	0.9898	0.232	0.20
13	1.0709	0.244	0.20
14	1.1520	0.256	0.20
15	1.2331	0.268	0.20
16	1.3142	0.280	0.20
17	1.3953	0.292	0.20
18	1.4764	0.304	0.20
19	1.5575	0.316	0.20
20	1.6386	0.328	0.20

AGE GROUP	TOTAL BICASS LOST	CONTRIBUTION TO CATCH PERCENT
1	0.2715	0.1281
2	0.4524	0.2041
3	0.6333	0.2801
4	0.8142	0.3561
5	0.9951	0.4321
6	1.1760	0.5081
7	1.3569	0.5841
8	1.5378	0.6601
9	1.7187	0.7361
10	1.8996	0.8121
11	2.0805	0.8881
12	2.2614	0.9641
13	2.4423	1.0401
14	2.6232	1.1161
15	2.8041	1.1921
16	2.9850	1.2681
17	3.1659	1.3441
18	3.3468	1.4201
19	3.5277	1.4961
20	3.7086	1.5721

THE ANNUAL YIELD IS 26.768 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.7544E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.2076E 07
 THE RATIO OF EGGS MATCHING TO EGGS SPAWNED IS 0.2976E-05

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1077	0.100	0.20
2	0.1788	0.112	0.20
3	0.2599	0.124	0.20
4	0.3410	0.136	0.20
5	0.4221	0.148	0.20
6	0.5032	0.160	0.20
7	0.5843	0.172	0.20
8	0.6654	0.184	0.20
9	0.7465	0.196	0.20
10	0.8276	0.208	0.20
11	0.9087	0.220	0.20
12	0.9898	0.232	0.20
13	1.0709	0.244	0.20
14	1.1520	0.256	0.20
15	1.2331	0.268	0.20
16	1.3142	0.280	0.20
17	1.3953	0.292	0.20
18	1.4764	0.304	0.20
19	1.5575	0.316	0.20
20	1.6386	0.328	0.20

AGE GROUP	TOTAL BICASS LOST	CONTRIBUTION TO CATCH PERCENT
1	0.2715	0.1281
2	0.4524	0.2041
3	0.6333	0.2801
4	0.8142	0.3561
5	0.9951	0.4321
6	1.1760	0.5081
7	1.3569	0.5841
8	1.5378	0.6601
9	1.7187	0.7361
10	1.8996	0.8121
11	2.0805	0.8881
12	2.2614	0.9641
13	2.4423	1.0401
14	2.6232	1.1161
15	2.8041	1.1921
16	2.9850	1.2681
17	3.1659	1.3441
18	3.3468	1.4201
19	3.5277	1.4961
20	3.7086	1.5721

THE ANNUAL YIELD IS 27.145 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.8075E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.2006E 07
 THE RATIO OF EGGS MATCHING TO EGGS SPAWNED IS 0.3948E-05

YEAR 1970

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0.0000	0.0000	0.1000	0.2000
0.0001	0.0001	0.1000	0.2000
0.0002	0.0002	0.1000	0.2000
0.0003	0.0003	0.1000	0.2000
0.0004	0.0004	0.1000	0.2000
0.0005	0.0005	0.1000	0.2000
0.0006	0.0006	0.1000	0.2000
0.0007	0.0007	0.1000	0.2000
0.0008	0.0008	0.1000	0.2000
0.0009	0.0009	0.1000	0.2000
0.0010	0.0010	0.1000	0.2000
0.0011	0.0011	0.1000	0.2000
0.0012	0.0012	0.1000	0.2000
0.0013	0.0013	0.1000	0.2000
0.0014	0.0014	0.1000	0.2000
0.0015	0.0015	0.1000	0.2000
0.0016	0.0016	0.1000	0.2000
0.0017	0.0017	0.1000	0.2000
0.0018	0.0018	0.1000	0.2000
0.0019	0.0019	0.1000	0.2000
0.0020	0.0020	0.1000	0.2000
0.0021	0.0021	0.1000	0.2000
0.0022	0.0022	0.1000	0.2000
0.0023	0.0023	0.1000	0.2000
0.0024	0.0024	0.1000	0.2000
0.0025	0.0025	0.1000	0.2000

AGE GROUP	TOTAL BIRTHS	LCST	CONTRIBUTION TO CATCH
0.0000	0.1821	0.0000	0.0000
0.0001	0.1441	0.0000	0.0000
0.0002	0.1100	0.0000	0.0000
0.0003	0.0800	0.0000	0.0000
0.0004	0.0550	0.0000	0.0000
0.0005	0.0350	0.0000	0.0000
0.0006	0.0200	0.0000	0.0000
0.0007	0.0100	0.0000	0.0000
0.0008	0.0050	0.0000	0.0000
0.0009	0.0025	0.0000	0.0000
0.0010	0.0012	0.0000	0.0000
0.0011	0.0006	0.0000	0.0000
0.0012	0.0003	0.0000	0.0000
0.0013	0.0001	0.0000	0.0000
0.0014	0.0000	0.0000	0.0000
0.0015	0.0000	0.0000	0.0000
0.0016	0.0000	0.0000	0.0000
0.0017	0.0000	0.0000	0.0000
0.0018	0.0000	0.0000	0.0000
0.0019	0.0000	0.0000	0.0000
0.0020	0.0000	0.0000	0.0000
0.0021	0.0000	0.0000	0.0000
0.0022	0.0000	0.0000	0.0000
0.0023	0.0000	0.0000	0.0000
0.0024	0.0000	0.0000	0.0000
0.0025	0.0000	0.0000	0.0000

THE ANNUAL YIELD IS 24.315 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.23382 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1456 07

NUMERICAL PARTICLE TRAJECTORY PROGRAM
 FINITE ELEMENT DATA:

NUMBER OF NODES = 191 NUMBER OF TRIANGULAR ELEMENTS = 200

FIELD SIZE: XMIN = 0.2254E 00 YMIN = 0.7500E 00 XMAX = 0.5233E 01 YMAX = 0.5877E 01

PARAMETER ENTRY
 NUMBER OF TIME STEPS = 1 TIME STEP = 1.00000 DAY VELOCITY TIME STEP = 1.00000 DAY
 TDRY = 10. DAY TPLT = 200000. DAY SPLT = 0 JPLT = 1
 DRY = 0.00100 ISEED = 783688
 IPCND = 149 IOP = 0 ISTOP = 1000. DAY ISTOP = 1000. DAY
 IYR = 1 IYR = 1970 IYR = 1970
 PRINTING PARAMETERS
 IPR = 0.10000 IPR = 0.10000 IPR = 1.00000 IPR = 0.00000 IPR = 0.00000
 PARTICLE DATA
 NP = 0
 NET DRIFT DATA
 INET = 0 UNET = 1.00000 VNET = 1.00000

TOTAL NUMBER OF ADJACENT ELEMENTS 2780

- THIS IS ENTRY NUMBER 1 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 2 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 3 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 4 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 5 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 6 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 7 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 8 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 9 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 10 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 11 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 12 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 13 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 14 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 15 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 16 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 17 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 18 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 19 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 20 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 21 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 22 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 23 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 24 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 25 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 26 TO SUBROUTINE ADVDF.
- THIS IS ENTRY NUMBER 27 TO SUBROUTINE ADVDF.

THIS IS ENTRY NUMBER 29 TO SUBROUTINE ADVDF.
 THIS IS ENTRY NUMBER 29 TO SUBROUTINE ADVDF.
 THIS IS ENTRY NUMBER 30 TO SUBROUTINE ADVDF.
 THIS IS ENTRY NUMBER 31 TO SUBROUTINE ADVDF.

IT	TIME	DAY	PARTICLE BUDGET	NP	NRDM	NRCT	NDUT
NGRPS= 30, KLOC= 3.76775, VELOC= 2.50000, RADIUS= 0.50000							
IT = 1	TIME =	301.000 DAY	PARTICLE BUDGET	NP = 60	NRDM = 60	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.1268E 12	AND PLARVA ENTRY IS	0.4330E 11	FOR DAY 301			
THIS IS ENTRY NUMBER 32 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	302.000 DAY	PARTICLE BUDGET	NP = 90	NRDM = 90	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.4863E 07	AND PLARVA ENTRY IS	0.2431E 07	FOR DAY 301			
THIS IS ENTRY NUMBER 33 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	303.000 DAY	PARTICLE BUDGET	NP = 120	NRDM = 120	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.2431E 07	AND PLARVA ENTRY IS	0.1215E 07	FOR DAY 301			
THIS IS ENTRY NUMBER 34 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	304.000 DAY	PARTICLE BUDGET	NP = 150	NRDM = 150	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.1620E 07	AND PLARVA ENTRY IS	0.8100E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 35 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	305.000 DAY	PARTICLE BUDGET	NP = 180	NRDM = 180	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.1215E 07	AND PLARVA ENTRY IS	0.6076E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 36 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	306.000 DAY	PARTICLE BUDGET	NP = 210	NRDM = 210	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.9715E 06	AND PLARVA ENTRY IS	0.4858E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 37 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	307.000 DAY	PARTICLE BUDGET	NP = 240	NRDM = 240	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.8094E 06	AND PLARVA ENTRY IS	0.4047E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 38 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	308.000 DAY	PARTICLE BUDGET	NP = 270	NRDM = 270	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.6926E 06	AND PLARVA ENTRY IS	0.3463E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 39 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	309.000 DAY	PARTICLE BUDGET	NP = 300	NRDM = 300	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.6067E 06	AND PLARVA ENTRY IS	0.3034E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 40 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	310.000 DAY	PARTICLE BUDGET	NP = 330	NRDM = 330	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.5381E 06	AND PLARVA ENTRY IS	0.2691E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 41 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	311.000 DAY	PARTICLE BUDGET	NP = 360	NRDM = 360	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.4851E 06	AND PLARVA ENTRY IS	0.2425E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 42 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	312.000 DAY	PARTICLE BUDGET	NP = 390	NRDM = 390	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.4400E 06	AND PLARVA ENTRY IS	0.2204E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 43 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	313.000 DAY	PARTICLE BUDGET	NP = 420	NRDM = 420	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.4040E 06	AND PLARVA ENTRY IS	0.2020E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 44 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	314.000 DAY	PARTICLE BUDGET	NP = 450	NRDM = 450	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.3720E 06	AND PLARVA ENTRY IS	0.1864E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 45 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	315.000 DAY	PARTICLE BUDGET	NP = 480	NRDM = 480	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.3461E 06	AND PLARVA ENTRY IS	0.1731E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 46 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	316.000 DAY	PARTICLE BUDGET	NP = 510	NRDM = 510	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.3230E 06	AND PLARVA ENTRY IS	0.1615E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 47 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	317.000 DAY	PARTICLE BUDGET	NP = 540	NRDM = 540	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.3027E 06	AND PLARVA ENTRY IS	0.1513E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 48 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	318.000 DAY	PARTICLE BUDGET	NP = 570	NRDM = 570	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.2848E 06	AND PLARVA ENTRY IS	0.1424E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 49 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	319.000 DAY	PARTICLE BUDGET	NP = 600	NRDM = 600	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.2689E 06	AND PLARVA ENTRY IS	0.1345E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 50 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	320.000 DAY	PARTICLE BUDGET	NP = 630	NRDM = 630	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			
LRYSUM IS	0.2547E 06	AND PLARVA ENTRY IS	0.1275E 06	FOR DAY 301			
THIS IS ENTRY NUMBER 51 TO SUBROUTINE ADVDF.							
IT = 1	TIME =	321.000 DAY	PARTICLE BUDGET	NP = 660	NRDM = 660	NRCT = 0	NDUT = 0
EP	EP	VP	IELP ITRPS ITRPE	SCRIPT			


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IT = 1   TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1390  NROW= 1390  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.894E 05 FOR DAY 301
THIS IS ENTRY NUMBER 75 TO SUBROUTINE ADVDTF.
TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1390  NROW= 1390  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.894E 05 FOR DAY 301
THIS IS ENTRY NUMBER 76 TO SUBROUTINE ADVDTF.
TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1410  NROW= 1410  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.894E 05 FOR DAY 301
THIS IS ENTRY NUMBER 77 TO SUBROUTINE ADVDTF.
TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1440  NROW= 1440  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.893E 05 FOR DAY 301
THIS IS ENTRY NUMBER 78 TO SUBROUTINE ADVDTF.
TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1470  NROW= 1470  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.893E 05 FOR DAY 301
THIS IS ENTRY NUMBER 79 TO SUBROUTINE ADVDTF.
TIME = 364,000 DAY   PARTICLE BUDGET:  NP = 1500  NROW= 1500  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.892E 05 FOR DAY 301

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TODAY IS 350 IT HAS BEEN 06 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 1
SPILLET  FLOC  VLOC  RADIUS
          3.4000  2.60700  0.0019
TODAY IS 350 AND THE VALUES OF KOILM,KOILNR,VOILM,VOILNR ARE 3.981 3.982 2.673 2.675
THE MAXIMUM SUBSURFACE CONCENTRATION IS 0000000000 PARTS PER BILLION ABOVE BACKGROUND LEVELS.
THERE ARE 137 ELEMENTS OUT THERE, WITH GRID SPACING DX,DY = 0.330E-04 0.403E-04METERS.
THIS IS ENTRY NUMBER 80 TO SUBROUTINE ADVDTF.
TIME = 350,000 DAY   PARTICLE BUDGET:  NP = 1530  NROW= 1530  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT

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HERE IS THE DISTRIBUTION PER DAY 350
DOY  350 1 30000 DISTRIBUTION WRITTEN TO DISC.

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DAY 351 TIME = 351,000 DAY   PARTICLE BUDGET:  NP = 1530  NROW= 1530  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.892E 05 FOR DAY 301
TODAY IS 351 IT HAS BEEN 07 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 2

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SPILLET  FLOC  VLOC  RADIUS
          3.4000  2.60700  0.0019
TODAY IS 351 AND THE VALUES OF KOILM,KOILNR,VOILM,VOILNR ARE 3.977 3.977 2.904 2.972
THE MAXIMUM SUBSURFACE CONCENTRATION IS 120415.25 PARTS PER BILLION ABOVE BACKGROUND LEVELS.
THERE ARE 137 ELEMENTS OUT THERE, WITH GRID SPACING DX,DY = 0.330E-04 0.403E-04METERS.
THIS IS ENTRY NUMBER 81 TO SUBROUTINE ADVDTF.
TIME = 351,000 DAY   PARTICLE BUDGET:  NP = 1560  NROW= 1560  NACT= 0  NOUT= 0
EP      EP      VP      TELP  STNPS  STNPE  SCRIPT
LEVSUM IS 0.170E 06 AND PLARYA ENTRY IS 0.891E 05 FOR DAY 301
TODAY IS 352 IT HAS BEEN 08 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 3

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SPILLET  FLOC  VLOC  RADIUS
          3.4000  2.60700  0.0019
TODAY IS 352 AND THE VALUES OF KOILM,KOILNR,VOILM,VOILNR ARE 3.941 4.055 2.910 2.981

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THE MAXIMUM SUBSURFACE CONCENTRATION IS 27994.00 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 61 ELEMENTS CUT THERE, WITH GRID SPACING DX,DY = 0.116E-01 0.116E-01 MAP UNITS.

THIS IS ENTRY NUMBER 02 TO SUBROUTINE ADV01F.

IT	TIME	IP	SP	VP	TELP	ITMPS	ITMPE	SCMPT	NP	NMOM	NACT	NOUT
1	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
2	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
3	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
4	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
5	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
6	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
7	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
8	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
9	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
10	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1

IDAY IS 353 IT HAS BEEN 353 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 4

SPILLET	RLOC	YLOC	RADIUS	U-DIST
1	3.524	3.524	0.079	0.079
2	3.524	3.524	0.079	0.079
3	3.524	3.524	0.079	0.079
4	3.524	3.524	0.079	0.079

IDAY IS 353 AND THE VALUES OF XOLM,XOLM,XOLM,XOLM ARE 3.629 4.143 2.573 2.837

THE MAXIMUM SUBSURFACE CONCENTRATION IS 28998.00 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 58 ELEMENTS CUT THERE, WITH GRID SPACING DX,DY = 0.101E-01 0.077E-01 MAP UNITS.

THIS IS ENTRY NUMBER 03 TO SUBROUTINE ADV01F.

IT	TIME	IP	SP	VP	TELP	ITMPS	ITMPE	SCMPT	NP	NMOM	NACT	NOUT
1	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
2	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
3	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
4	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
5	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
6	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
7	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
8	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
9	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1
10	3.524	3.524	0.120	17	108	346	0	F	1610	1610	0	1

IDAY IS 354 IT HAS BEEN 354 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 5

SPILLET	RLOC	YLOC	RADIUS	U-DIST
1	3.524	3.524	0.079	0.079
2	3.524	3.524	0.079	0.079
3	3.524	3.524	0.079	0.079
4	3.524	3.524	0.079	0.079
5	3.524	3.524	0.079	0.079

IDAY IS 354 AND THE VALUES OF XOLM,XOLM,XOLM,XOLM ARE 3.633 4.301 2.544 2.801

THE MAXIMUM SUBSURFACE CONCENTRATION IS 12098.77 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 113 ELEMENTS CUT THERE, WITH GRID SPACING DX,DY = 0.248E-01 0.042E-02 MAP UNITS.

THIS IS ENTRY NUMBER 04 TO SUBROUTINE ADV01F.

IT	TIME	IP	SP	VP	TELP	ITMPS	ITMPE	SCMPT	NP	NMOM	NACT	NOUT
1	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
2	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
3	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
4	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
5	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
6	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
7	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
8	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
9	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1
10	3.524	3.524	0.120	17	108	346	0	F	1645	1645	0	1

IDAY IS 355 IT HAS BEEN 355 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 6

SPILLET	RLOC	YLOC	RADIUS	U-DIST
1	3.524	3.524	0.079	0.079
2	3.524	3.524	0.079	0.079
3	3.524	3.524	0.079	0.079
4	3.524	3.524	0.079	0.079
5	3.524	3.524	0.079	0.079
6	3.524	3.524	0.079	0.079

IDAY IS 355 AND THE VALUES OF XOLM,XOLM,XOLM,XOLM ARE 3.614 4.400 2.471 2.716

THE MAXIMUM SUBSURFACE CONCENTRATION IS 16827.57 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 111 ELEMENTS CUT THERE, WITH GRID SPACING DX,DY = 0.293E-01 0.006E-02 MAP UNITS.

THIS IS ENTRY NUMBER 05 TO SUBROUTINE ADV01F.

IT	TIME	IP	SP	VP	TELP	ITMPS	ITMPE	SCMPT	NP	NMOM	NACT	NOUT
1	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
2	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
3	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
4	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
5	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
6	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
7	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
8	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
9	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4
10	3.524	3.524	0.120	17	108	346	0	F	1668	1668	0	4

IDAY IS 356 IT HAS BEEN 356 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETS IS 7

SPILLET	RLOC	YLOC	RADIUS	U-DIST
1	3.524	3.524	0.079	0.079
2	3.524	3.524	0.079	0.079
3	3.524	3.524	0.079	0.079
4	3.524	3.524	0.079	0.079
5	3.524	3.524	0.079	0.079
6	3.524	3.524	0.079	0.079
7	3.524	3.524	0.079	0.079

IDAY IS 356 AND THE VALUES OF XOLM,XOLM,XOLM,XOLM ARE 3.590 4.404 2.497 2.737

THE MAXIMUM SUBSURFACE CONCENTRATION IS 11026.57 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 123 ELEMENTS CUT THERE, WITH GRID SPACING DX,DY = 0.299E-01 0.006E-02 MAP UNITS.

THIS IS ENTRY NUMBER 86 TO SUPERFICIAL ADVDP.
IT = 1 PARTICLE OUTSIDE TIME = 356.0000 DAY

IP	SP	VP	TELP	ITMPS	ITMPE	SCNPT
33	0.27790	0.74400	107	301	356	F
34	0.88000	0.50272	107	301	356	F
35	0.85100	0.88000	107	301	356	F
36	0.95375	0.58800	107	301	356	F
37	0.92700	0.37074	107	301	356	F
38	0.89200	0.37074	107	301	356	F
39	0.92000	0.10170	107	301	356	F
40	0.98400	0.38200	107	301	356	F
41	0.94700	0.51000	107	301	356	F
42	0.90170	0.47122	107	301	356	F

EVSUM IS 0.16700 DS AND PLARY ENTRY IS 0.8408E DS FOR DAY 301

DAY IS 351 IT HAS BEEN 76 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETTS IS 8

SPILLET	RLOC	VLOC	RADIUS
1	4.0300	2.3977	0.0391
2	4.2157	2.5500	0.0390
3	4.2157	2.5500	0.0391
4	4.2157	2.5500	0.0390
5	4.2157	2.5500	0.0391
6	4.2157	2.5500	0.0390
7	4.2157	2.5500	0.0391
8	4.2157	2.5500	0.0390

DAY IS 357 AND THE VALUES OF KOILM,KOILM,KOILM,KOILM ARE 3.572 4.393 2.478 2.716

THE MAXIMUM SURFACE CONCENTRATION IS 14820.90 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 162 ELEMENTS OUT THERE, WITH GRID SPACING DELTA X = 0.305E-01 0.882E-02 MAP UNITS.

THIS IS ENTRY NUMBER 87 TO SUPERFICIAL ADVDP.
IT = 1 PARTICLE OUTSIDE TIME = 357.0000 DAY

IP	SP	VP	TELP	ITMPS	ITMPE	SCNPT
34	0.27790	0.74400	107	301	357	F
35	0.88000	0.50272	107	301	357	F
36	0.85100	0.88000	107	301	357	F
37	0.95375	0.58800	107	301	357	F
38	0.92700	0.37074	107	301	357	F
39	0.89200	0.37074	107	301	357	F
40	0.92000	0.10170	107	301	357	F
41	0.98400	0.38200	107	301	357	F
42	0.94700	0.51000	107	301	357	F
43	0.90170	0.47122	107	301	357	F

EVSUM IS 0.16700 DS AND PLARY ENTRY IS 0.8408E DS FOR DAY 301

DAY IS 358 IT HAS BEEN 80 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETTS IS 9

SPILLET	RLOC	VLOC	RADIUS
1	4.1184	2.4378	0.0391
2	4.1884	2.5090	0.0380
3	4.2171	2.4138	0.0390
4	4.0455	2.4378	0.0391
5	3.5270	2.4378	0.0391
6	3.5270	2.4378	0.0392
7	3.5270	2.4378	0.0391
8	3.5270	2.4378	0.0392
9	3.5270	2.4378	0.0391

DAY IS 358 AND THE VALUES OF KOILM,KOILM,KOILM,KOILM ARE 3.542 4.378 2.436 2.706

THE MAXIMUM SUBSURFACE CONCENTRATION IS 9401.00 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 143 ELEMENTS OUT THERE, WITH GRID SPACING DELTA X = 0.310E-01 0.132E-01 MAP UNITS.

THIS IS ENTRY NUMBER 88 TO SUPERFICIAL ADVDP.
IT = 1 PARTICLE OUTSIDE TIME = 358.0000 DAY

IP	SP	VP	TELP	ITMPS	ITMPE	SCNPT
35	0.27790	0.74400	108	301	358	F
36	0.88000	0.50272	107	301	358	F
37	0.85100	0.88000	107	301	358	F
38	0.95375	0.58800	107	301	358	F
39	0.92700	0.37074	107	301	358	F
40	0.89200	0.37074	107	301	358	F
41	0.92000	0.10170	107	301	358	F
42	0.98400	0.38200	107	301	358	F
43	0.94700	0.51000	107	301	358	F
44	0.90170	0.47122	107	301	358	F

EVSUM IS 0.1640E DS AND PLARY ENTRY IS 0.8484E DS FOR DAY 301

DAY IS 359 IT HAS BEEN 84 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETTS IS 10

SPILLET	RLOC	VLOC	RADIUS
1	4.2372	2.4378	0.0391
2	4.4000	2.4378	0.0390
3	4.2372	2.4378	0.0390
4	4.1782	2.5200	0.0401
5	4.1878	2.3377	0.0391
6	4.1878	2.3377	0.0391
7	4.2372	2.3377	0.0391
8	4.2372	2.3377	0.0391
9	4.2372	2.3377	0.0391
10	4.2372	2.3377	0.0391

DAY IS 359 AND THE VALUES OF KOILM,KOILM,KOILM,KOILM ARE 3.499 4.294 2.330 2.720

THE MAXIMUM SUBSURFACE CONCENTRATION IS 7224.43 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 129 ELEMENTS OUT THERE, WITH GRID SPACING DELTA X = 0.319E-01 0.150E-01 MAP UNITS.

THIS IS ENTRY NUMBER 89 TO SUPERFICIAL ADVDP.
IT = 1 PARTICLE OUTSIDE TIME = 359.0000 DAY

IP	SP	VP	TELP	ITMPS	ITMPE	SCNPT
36	0.27790	0.74400	108	301	359	F
37	0.88000	0.50272	107	301	359	F
38	0.85100	0.88000	107	301	359	F
39	0.95375	0.58800	107	301	359	F
40	0.92700	0.37074	107	301	359	F
41	0.89200	0.37074	107	301	359	F
42	0.92000	0.10170	107	301	359	F
43	0.98400	0.38200	107	301	359	F
44	0.94700	0.51000	107	301	359	F
45	0.90170	0.47122	107	301	359	F

EVSUM IS 0.1640E DS AND PLARY ENTRY IS 0.8484E DS FOR DAY 301

HERE IS THE DISTRIBUTION FOR DAY 105

BAR BAR LARVAL DISTRIBUTION WRITING TO DISC

DAY 105 0.2247E 05 AND PLARYA ENTRY IS 0.5305E 05 FOR DAY 341
 LRVSUM IS 0.3253E 05 AND PLARYA ENTRY IS 0.5784E 05 FOR DAY 351

DAY IS 470 IT HAS BEEN 120 DAYS SINCE THE SPILL. THE NUMBER OF SPILLETTS IS 30

SPILLET	RLOC	VLOC	RADIUS
1	0.3167	-2.0200	0.0316
2	0.3167	-2.1604	0.0316
3	0.3167	-2.3008	0.0316
4	0.3167	-2.4412	0.0316
5	0.3167	-2.5816	0.0316
6	0.3167	-2.7220	0.0316
7	0.3167	-2.8624	0.0316
8	0.3167	-3.0028	0.0316
9	0.3167	-3.1432	0.0316
10	0.3167	-3.2836	0.0316
11	0.3167	-3.4240	0.0316
12	0.3167	-3.5644	0.0316
13	0.3167	-3.7048	0.0316
14	0.3167	-3.8452	0.0316
15	0.3167	-3.9856	0.0316
16	0.3167	-4.1260	0.0316
17	0.3167	-4.2664	0.0316
18	0.3167	-4.4068	0.0316
19	0.3167	-4.5472	0.0316
20	0.3167	-4.6876	0.0316
21	0.3167	-4.8280	0.0316
22	0.3167	-4.9684	0.0316
23	0.3167	-5.1088	0.0316
24	0.3167	-5.2492	0.0316
25	0.3167	-5.3896	0.0316
26	0.3167	-5.5300	0.0316
27	0.3167	-5.6704	0.0316
28	0.3167	-5.8108	0.0316
29	0.3167	-5.9512	0.0316
30	0.3167	-6.0916	0.0316

DAY IS 106 AND THE VALUES OF KOLMA, KOLMA, YOILMA, YOILMA ARE 2.159 5.419 2.376 3.033
 THE MAXIMUM SUBSURFACE CONCENTRATION IS 3153.00 PARTS PER BILLION ABOVE BACKGROUND LEVELS.

THERE ARE 49 ELEMENTS OUT THERE WITH GRID SPACING OF 0.0171E 05 OR 0.2621-GRID UNITS.

THIS IS ENTRY NUMBER 200 TO SUBROUTINE ADVIS.

TIME	TIME	100,000 DAY	PARTICLE	NUDCPTI	NP	1184	NNON	1104	NRCT	0	ROUT	750
1	1.2347	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
2	1.0974	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
3	0.9608	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
4	0.8242	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
5	0.6876	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
6	0.5510	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
7	0.4144	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
8	0.2778	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
9	0.1412	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974
10	0.0046	2.2300	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974	1.0974

TP	RP	VP	TEP	TYPS	TYPE	SCRIPT
138	1.23467	2.23079	98	100	100	F
139	1.09242	2.23079	97	100	100	F
140	0.94960	2.23079	96	100	100	F
141	0.80678	2.23079	95	100	100	F
142	0.66396	2.23079	94	100	100	F
143	0.52114	2.23079	93	100	100	F
144	0.37832	2.23079	92	100	100	F
145	0.23550	2.23079	91	100	100	F
146	0.09268	2.23079	90	100	100	F
147	0.00000	2.23079	89	100	100	F

THE CYCSPLE BEGINS ON DAY 350, AND ITS DIRECT EFFECTS ON THE FISHERY ENDED ON DAY 107.

THIS IS ENTRY NUMBER 201 TO SUBROUTINE ADVIS.

TIME	TIME	100,000 DAY	PARTICLE	NUDCPTI	NP	1101	NNON	1193	NRCT	0	ROUT	720
1	1.2346	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
2	1.0966	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
3	0.9590	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
4	0.8214	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
5	0.6838	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
6	0.5462	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
7	0.4086	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
8	0.2710	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
9	0.1334	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966
10	0.0000	2.2800	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966	1.0966

TP	RP	VP	TEP	TYPS	TYPE	SCRIPT
148	1.23467	2.28027	89	102	102	F
149	1.09242	2.28027	88	102	102	F
150	0.94960	2.28027	87	102	102	F
151	0.80678	2.28027	86	102	102	F
152	0.66396	2.28027	85	102	102	F
153	0.52114	2.28027	84	102	102	F
154	0.37832	2.28027	83	102	102	F
155	0.23550	2.28027	82	102	102	F
156	0.09268	2.28027	81	102	102	F
157	0.00000	2.28027	80	102	102	F

YEAR 1961

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.0000	0.1000	0.2000
1	0.0000	0.1000	0.2000
2	0.0000	0.1000	0.2000
3	0.0000	0.1000	0.2000
4	0.0000	0.1000	0.2000
5	0.0000	0.1000	0.2000
6	0.0000	0.1000	0.2000
7	0.0000	0.1000	0.2000
8	0.0000	0.1000	0.2000
9	0.0000	0.1000	0.2000
10	0.0000	0.1000	0.2000
11	0.0000	0.1000	0.2000
12	0.0000	0.1000	0.2000
13	0.0000	0.1000	0.2000
14	0.0000	0.1000	0.2000
15	0.0000	0.1000	0.2000
16	0.0000	0.1000	0.2000
17	0.0000	0.1000	0.2000
18	0.0000	0.1000	0.2000
19	0.0000	0.1000	0.2000
20	0.0000	0.1000	0.2000

AGE GROUP	TOTAL WEIGHTS LOST	CONTRIBUTION TO CATCH
0	0.1835E 07	0.8284E 06
1	0.1465E 07	0.6567E 06
2	0.1105E 07	0.5000E 06
3	0.8455E 06	0.3800E 06
4	0.6500E 06	0.2900E 06
5	0.4950E 06	0.2200E 06
6	0.3750E 06	0.1700E 06
7	0.2850E 06	0.1300E 06
8	0.2150E 06	0.1000E 06
9	0.1650E 06	0.0750E 06
10	0.1250E 06	0.0550E 06
11	0.0950E 06	0.0400E 06
12	0.0700E 06	0.0300E 06
13	0.0500E 06	0.0200E 06
14	0.0350E 06	0.0150E 06
15	0.0250E 06	0.0100E 06
16	0.0180E 06	0.0070E 06
17	0.0130E 06	0.0050E 06
18	0.0090E 06	0.0040E 06
19	0.0060E 06	0.0030E 06
20	0.0040E 06	0.0020E 06

THE ANNUAL YIELD IS 21.471 TONS AND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.5510E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.191E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANDED IS 0.3075E-05

YEAR 1982

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.17741 C9	0.311	0.70
2	0.84341 C7	0.311	0.70
3	0.36471 C7	0.311	0.70
4	0.26751 C7	0.311	0.70
5	0.19331 C7	0.311	0.70
6	0.12101 C7	0.311	0.70
7	0.84341 C6	0.311	0.70
8	0.36471 C6	0.311	0.70
9	0.26751 C6	0.311	0.70
10	0.19331 C6	0.311	0.70
11	0.12101 C6	0.311	0.70
12	0.84341 C5	0.311	0.70
13	0.36471 C5	0.311	0.70
14	0.26751 C5	0.311	0.70
15	0.19331 C5	0.311	0.70
16	0.12101 C5	0.311	0.70

AGE GROUP	TOTAL BIRCHASS LOST	CONTRIBUTION TO CATCH PERCENT
1	0.3112E 07	0.14451 C7
2	0.3240E 07	0.2002E 07
3	0.1678E 07	0.2210E 07
4	0.1240E 07	0.2210E 07
5	0.3240E 07	0.2002E 07
6	0.2747E 07	0.1524E 07
7	0.1240E 07	0.2210E 07
8	0.1141E 07	0.2204E 06
9	0.4135E 06	0.2204E 06
10	0.5373E 06	0.2311E 06
11	0.1191E 06	0.2311E 06
12	0.3790E 06	0.2003E 06
13	0.7453E 06	0.4840E 06

THE ANNUAL YIELD IS 20.361 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4741E 17
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.192E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNEC IS 0.4273E-04

YEAR 1983

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.17741 C9	0.310	0.70
2	0.84341 C7	0.310	0.70
3	0.36471 C7	0.310	0.70
4	0.26751 C7	0.310	0.70
5	0.19331 C7	0.310	0.70
6	0.12101 C7	0.310	0.70
7	0.84341 C6	0.310	0.70
8	0.36471 C6	0.310	0.70
9	0.26751 C6	0.310	0.70
10	0.19331 C6	0.310	0.70
11	0.12101 C6	0.310	0.70
12	0.84341 C5	0.310	0.70
13	0.36471 C5	0.310	0.70
14	0.26751 C5	0.310	0.70
15	0.19331 C5	0.310	0.70
16	0.12101 C5	0.310	0.70

AGE GROUP	TOTAL BIRCHASS LOST	CONTRIBUTION TO CATCH PERCENT
1	0.1678E 07	0.1390E 07
2	0.2747E 07	0.1020E 07
3	0.2041E 07	0.1410E 07
4	0.1401E 07	0.1888E 07
5	0.2747E 07	0.1888E 07
6	0.2041E 07	0.1737E 07
7	0.1401E 07	0.1344E 07
8	0.1131E 07	0.1285E 07
9	0.1737E 07	0.1344E 07
10	0.1131E 07	0.1037E 06
11	0.1005E 07	0.1037E 06
12	0.2514E 06	0.3424E 06
13	0.4270E 06	0.2995E 06
14	0.1124E 06	0.1944E 06
15	0.2218E 06	0.2434E 06
16	0.4647E 06	0.3676E 06

THE ANNUAL YIELD IS 18.040 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4107E 17
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.191E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNEC IS 0.4930E-04

YEAR 1984

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.17741 C9	0.303	0.70
2	0.84341 C7	0.303	0.70
3	0.36471 C7	0.303	0.70
4	0.26751 C7	0.303	0.70
5	0.19331 C7	0.303	0.70
6	0.12101 C7	0.303	0.70
7	0.84341 C6	0.303	0.70
8	0.36471 C6	0.303	0.70
9	0.26751 C6	0.303	0.70
10	0.19331 C6	0.303	0.70
11	0.12101 C6	0.303	0.70
12	0.84341 C5	0.303	0.70
13	0.36471 C5	0.303	0.70
14	0.26751 C5	0.303	0.70
15	0.19331 C5	0.303	0.70
16	0.12101 C5	0.303	0.70

AGE GROUP	TOTAL BIRCHASS LOST	CONTRIBUTION TO CATCH PERCENT
1	0.1678E 07	0.1091E 07
2	0.2041E 07	0.2659E 07
3	0.1401E 07	0.1858E 07
4	0.1005E 07	0.1400E 07
5	0.2041E 07	0.1400E 07
6	0.1401E 07	0.1102E 07
7	0.1102E 07	0.1102E 07
8	0.1401E 07	0.1102E 07
9	0.1102E 07	0.1102E 07
10	0.1102E 07	0.1102E 07
11	0.1102E 07	0.1102E 07
12	0.2747E 06	0.4037E 06
13	0.4647E 06	0.4037E 06
14	0.1102E 06	0.1102E 06
15	0.2218E 06	0.2218E 06
16	0.4647E 06	0.3218E 06

THE ANNUAL YIELD IS 18.001 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3600E 17
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.188E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNEC IS 0.5610E-04

			YEAR 1985	
AGE GROUP	SIZE		FISHING MORTALITY	NATURAL MORTALITY
	0.1374E 08		0.0000	0.0000
	0.2556E 07		0.0000	0.0000
	0.5751E 07		0.0000	0.0000
	0.2457E 07		0.0000	0.0000
	0.7287E 06		0.0000	0.0000
	0.2982E 06		0.0000	0.0000
	0.2074E 06		0.0000	0.0000
	0.1847E 06		0.0000	0.0000
	0.5723E 05		0.0000	0.0000
	0.3947E 05		0.0000	0.0000
	0.2000E 05		0.0000	0.0000
	0.5324E 04		0.0000	0.0000

AGE GROUP	TOTAL	BIOMASS LOST	CONTRIBUTION TO CATCH	PERCENT
	0.4470E 07	0.0000	0.0000	0.0000
	0.5295E 07	0.0000	0.0000	0.0000
	0.4653E 07	0.0000	0.0000	0.0000
	0.2425E 07	0.0000	0.0000	0.0000
	0.3102E 07	0.0000	0.0000	0.0000
	0.1849E 07	0.0000	0.0000	0.0000
	0.1350E 07	0.0000	0.0000	0.0000
	0.1847E 06	0.0000	0.0000	0.0000
	0.5627E 06	0.0000	0.0000	0.0000
	0.4575E 06	0.0000	0.0000	0.0000
	0.3088E 06	0.0000	0.0000	0.0000
	0.1780E 06	0.0000	0.0000	0.0000
	0.1489E 06	0.0000	0.0000	0.0000
	0.4671E 05	0.0000	0.0000	0.0000

THE ANNUAL YIELD IS 18.523 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3424E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1866E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.4943E-05

			YEAR 1986	
AGE GROUP	SIZE		FISHING MORTALITY	NATURAL MORTALITY
	0.1374E 08		0.0000	0.0000
	0.2556E 07		0.0000	0.0000
	0.5751E 07		0.0000	0.0000
	0.2457E 07		0.0000	0.0000
	0.7287E 06		0.0000	0.0000
	0.2982E 06		0.0000	0.0000
	0.2074E 06		0.0000	0.0000
	0.1847E 06		0.0000	0.0000
	0.5723E 05		0.0000	0.0000
	0.3947E 05		0.0000	0.0000
	0.2000E 05		0.0000	0.0000
	0.5324E 04		0.0000	0.0000

AGE GROUP	TOTAL	BIOMASS LOST	CONTRIBUTION TO CATCH	PERCENT
	0.3167E 07	0.0000	0.0000	0.0000
	0.5073E 07	0.0000	0.0000	0.0000
	0.4472E 07	0.0000	0.0000	0.0000
	0.2425E 07	0.0000	0.0000	0.0000
	0.2018E 07	0.0000	0.0000	0.0000
	0.1849E 07	0.0000	0.0000	0.0000
	0.1778E 07	0.0000	0.0000	0.0000
	0.1847E 06	0.0000	0.0000	0.0000
	0.6070E 06	0.0000	0.0000	0.0000
	0.5724E 06	0.0000	0.0000	0.0000
	0.3746E 06	0.0000	0.0000	0.0000
	0.2756E 06	0.0000	0.0000	0.0000
	0.4088E 06	0.0000	0.0000	0.0000
	0.1489E 06	0.0000	0.0000	0.0000
	0.3907E 05	0.0000	0.0000	0.0000

THE ANNUAL YIELD IS 19.218 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3674E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1594E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.4904E-05

			YEAR 1987	
AGE GROUP	SIZE		FISHING MORTALITY	NATURAL MORTALITY
	0.1374E 08		0.0000	0.0000
	0.2556E 07		0.0000	0.0000
	0.5751E 07		0.0000	0.0000
	0.2457E 07		0.0000	0.0000
	0.7287E 06		0.0000	0.0000
	0.2982E 06		0.0000	0.0000
	0.2074E 06		0.0000	0.0000
	0.1847E 06		0.0000	0.0000
	0.5723E 05		0.0000	0.0000
	0.3947E 05		0.0000	0.0000
	0.2000E 05		0.0000	0.0000
	0.5324E 04		0.0000	0.0000

AGE GROUP	TOTAL	BIOMASS LOST	CONTRIBUTION TO CATCH	PERCENT
	0.2103E 07	0.0000	0.0000	0.0000
	0.3168E 07	0.0000	0.0000	0.0000
	0.2628E 07	0.0000	0.0000	0.0000
	0.4604E 07	0.0000	0.0000	0.0000
	0.3329E 07	0.0000	0.0000	0.0000
	0.3200E 07	0.0000	0.0000	0.0000
	0.1010E 07	0.0000	0.0000	0.0000
	0.7508E 06	0.0000	0.0000	0.0000
	0.6072E 06	0.0000	0.0000	0.0000
	0.5724E 06	0.0000	0.0000	0.0000
	0.3752E 06	0.0000	0.0000	0.0000
	0.2380E 06	0.0000	0.0000	0.0000
	0.1678E 06	0.0000	0.0000	0.0000
	0.3218E 06	0.0000	0.0000	0.0000
	0.1489E 06	0.0000	0.0000	0.0000
	0.3164E 05	0.0000	0.0000	0.0000

THE ANNUAL YIELD IS 19.238 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3720E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1494E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.4933E-05

YEAR 1988

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1174E C8	0.107	0.70
1	0.0473E C7	0.310	0.70
2	0.5214E C7	0.310	0.70
3	0.3308E C7	0.310	0.70
4	0.2011E C7	0.310	0.70
5	0.7214E C6	0.310	0.70
6	0.2211E C6	0.310	0.70
7	0.1471E C6	0.310	0.70
8	0.1737E C6	0.310	0.70
9	0.3804E C5	0.310	0.70
10	0.5607E C5	0.310	0.70
11	0.3804E C5	0.310	0.70
12	0.2451E C5	0.310	0.70
13	0.1921E C5	0.310	0.70
14	0.1431E C5	0.310	0.70
15	0.1071E C5	0.310	0.70

AGE GROUP	TOTAL BICHASS LOST (KG)	CONTRIBUTION TO CATCH PERCENT
0	0.310E C7	0.184E C7
1	0.4979E C7	0.3024E C7
2	0.4979E C7	0.3024E C7
3	0.4979E C7	0.3024E C7
4	0.4979E C7	0.3024E C7
5	0.2411E C7	0.1574E C7
6	0.2411E C7	0.1574E C7
7	0.2411E C7	0.1574E C7
8	0.2411E C7	0.1574E C7
9	0.1144E C6	0.0503E C6
10	0.0878E C6	0.0450E C6
11	0.1144E C6	0.0503E C6
12	0.2869E C6	0.0732E C6
13	0.1814E C6	0.0473E C6
14	0.2031E C6	0.0473E C6
15	0.1462E C6	0.0380E C6
16	0.1462E C6	0.0380E C6
17	0.1462E C6	0.0380E C6
18	0.1462E C6	0.0380E C6
19	0.1462E C6	0.0380E C6
20	0.1462E C6	0.0380E C6

THE ANNUAL YIELD IS 18.468 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3784E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANND IS 0.5351E-C5

YEAR 1989

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E C8	0.173	0.70
1	0.5214E C7	0.301	0.70
2	0.3308E C7	0.301	0.70
3	0.2011E C7	0.301	0.70
4	0.1271E C7	0.301	0.70
5	0.4376E C6	0.301	0.70
6	0.1503E C6	0.301	0.70
7	0.1503E C6	0.301	0.70
8	0.1503E C6	0.301	0.70
9	0.1503E C6	0.301	0.70
10	0.1503E C6	0.301	0.70
11	0.1503E C6	0.301	0.70
12	0.1503E C6	0.301	0.70
13	0.1503E C6	0.301	0.70
14	0.1503E C6	0.301	0.70
15	0.1503E C6	0.301	0.70
16	0.1503E C6	0.301	0.70
17	0.1503E C6	0.301	0.70
18	0.1503E C6	0.301	0.70
19	0.1503E C6	0.301	0.70
20	0.1503E C6	0.301	0.70

AGE GROUP	TOTAL BICHASS LOST (KG)	CONTRIBUTION TO CATCH PERCENT
0	0.310E C7	0.184E C7
1	0.4979E C7	0.3024E C7
2	0.4979E C7	0.3024E C7
3	0.4979E C7	0.3024E C7
4	0.4979E C7	0.3024E C7
5	0.2411E C7	0.1574E C7
6	0.2411E C7	0.1574E C7
7	0.2411E C7	0.1574E C7
8	0.2411E C7	0.1574E C7
9	0.1144E C6	0.0503E C6
10	0.0878E C6	0.0450E C6
11	0.1144E C6	0.0503E C6
12	0.2869E C6	0.0732E C6
13	0.1814E C6	0.0473E C6
14	0.2031E C6	0.0473E C6
15	0.1462E C6	0.0380E C6
16	0.1462E C6	0.0380E C6
17	0.1462E C6	0.0380E C6
18	0.1462E C6	0.0380E C6
19	0.1462E C6	0.0380E C6
20	0.1462E C6	0.0380E C6

THE ANNUAL YIELD IS 18.645 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3806E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANND IS 0.5237E-C5

YEAR 1990

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E C8	0.164	0.70
1	0.5214E C7	0.304	0.70
2	0.3308E C7	0.304	0.70
3	0.2011E C7	0.304	0.70
4	0.1271E C7	0.304	0.70
5	0.4376E C6	0.304	0.70
6	0.1503E C6	0.304	0.70
7	0.1503E C6	0.304	0.70
8	0.1503E C6	0.304	0.70
9	0.1503E C6	0.304	0.70
10	0.1503E C6	0.304	0.70
11	0.1503E C6	0.304	0.70
12	0.1503E C6	0.304	0.70
13	0.1503E C6	0.304	0.70
14	0.1503E C6	0.304	0.70
15	0.1503E C6	0.304	0.70
16	0.1503E C6	0.304	0.70
17	0.1503E C6	0.304	0.70
18	0.1503E C6	0.304	0.70
19	0.1503E C6	0.304	0.70
20	0.1503E C6	0.304	0.70

AGE GROUP	TOTAL BICHASS LOST (KG)	CONTRIBUTION TO CATCH PERCENT
0	0.310E C7	0.184E C7
1	0.4979E C7	0.3024E C7
2	0.4979E C7	0.3024E C7
3	0.4979E C7	0.3024E C7
4	0.4979E C7	0.3024E C7
5	0.2411E C7	0.1574E C7
6	0.2411E C7	0.1574E C7
7	0.2411E C7	0.1574E C7
8	0.2411E C7	0.1574E C7
9	0.1144E C6	0.0503E C6
10	0.0878E C6	0.0450E C6
11	0.1144E C6	0.0503E C6
12	0.2869E C6	0.0732E C6
13	0.1814E C6	0.0473E C6
14	0.2031E C6	0.0473E C6
15	0.1462E C6	0.0380E C6
16	0.1462E C6	0.0380E C6
17	0.1462E C6	0.0380E C6
18	0.1462E C6	0.0380E C6
19	0.1462E C6	0.0380E C6
20	0.1462E C6	0.0380E C6

THE ANNUAL YIELD IS 19.175 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.1961E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.195E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANND IS 0.9112E-C5

YEAR 1991

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
U.1374E C5	0.1374E C5	0.170	0.20
U.4922E C7	0.4922E C7	0.170	0.20
U.2013E C7	0.2013E C7	0.170	0.20
U.3084E C7	0.3084E C7	0.170	0.20
U.7272E C7	0.7272E C7	0.170	0.20
U.1737E C7	0.1737E C7	0.170	0.20
U.8434E C6	0.8434E C6	0.170	0.20
U.3462E C6	0.3462E C6	0.170	0.20
U.2412E C6	0.2412E C6	0.170	0.20
U.1631E C6	0.1631E C6	0.170	0.20
U.1013E C5	0.1013E C5	0.170	0.20
U.7111E C5	0.7111E C5	0.170	0.20
U.2777E C5	0.2777E C5	0.170	0.20
U.1721E C5	0.1721E C5	0.170	0.20
U.8481E C5	0.8481E C5	0.170	0.20
U.1936E C5	0.1936E C5	0.170	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH PERCENT
U.1374E C5	0.1374E C5	0.1460E C7
U.4922E C7	0.4922E C7	0.1184E C7
U.2013E C7	0.2013E C7	0.1213E C7
U.3084E C7	0.3084E C7	0.130E C7
U.7272E C7	0.7272E C7	0.126E C7
U.1737E C7	0.1737E C7	0.102E C7
U.8434E C6	0.8434E C6	0.059E C6
U.3462E C6	0.3462E C6	0.051E C6
U.2412E C6	0.2412E C6	0.051E C6
U.1631E C6	0.1631E C6	0.051E C6
U.1013E C5	0.1013E C5	0.051E C5
U.7111E C5	0.7111E C5	0.051E C5
U.2777E C5	0.2777E C5	0.051E C5
U.1721E C5	0.1721E C5	0.051E C5
U.8481E C5	0.8481E C5	0.051E C5
U.1936E C5	0.1936E C5	0.051E C5

THE ANNUAL YIELD IS 20.640 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.6205E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS MATCHING TO EGGS SPANNED IS 0.5300E-05

YEAR 1992

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
U.1374E C5	0.1374E C5	0.171	0.20
U.4922E C7	0.4922E C7	0.170	0.20
U.2013E C7	0.2013E C7	0.170	0.20
U.3084E C7	0.3084E C7	0.170	0.20
U.7272E C7	0.7272E C7	0.170	0.20
U.1737E C7	0.1737E C7	0.170	0.20
U.8434E C6	0.8434E C6	0.170	0.20
U.3462E C6	0.3462E C6	0.170	0.20
U.2412E C6	0.2412E C6	0.170	0.20
U.1631E C6	0.1631E C6	0.170	0.20
U.1013E C5	0.1013E C5	0.170	0.20
U.7111E C5	0.7111E C5	0.170	0.20
U.2777E C5	0.2777E C5	0.170	0.20
U.1721E C5	0.1721E C5	0.170	0.20
U.8481E C5	0.8481E C5	0.170	0.20
U.1936E C5	0.1936E C5	0.170	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH PERCENT
U.1374E C5	0.1374E C5	0.1474E C7
U.4922E C7	0.4922E C7	0.1064E C7
U.2013E C7	0.2013E C7	0.124E C7
U.3084E C7	0.3084E C7	0.124E C7
U.7272E C7	0.7272E C7	0.126E C7
U.1737E C7	0.1737E C7	0.102E C7
U.8434E C6	0.8434E C6	0.059E C6
U.3462E C6	0.3462E C6	0.051E C6
U.2412E C6	0.2412E C6	0.051E C6
U.1631E C6	0.1631E C6	0.051E C6
U.1013E C5	0.1013E C5	0.051E C5
U.7111E C5	0.7111E C5	0.051E C5
U.2777E C5	0.2777E C5	0.051E C5
U.1721E C5	0.1721E C5	0.051E C5
U.8481E C5	0.8481E C5	0.051E C5
U.1936E C5	0.1936E C5	0.051E C5

THE ANNUAL YIELD IS 19.840 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.5949E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.157E 07
 THE RATIO OF EGGS MATCHING TO EGGS SPANNED IS 0.5276E-05

YEAR 1993

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
U.1374E C5	0.1374E C5	0.162	0.20
U.4922E C7	0.4922E C7	0.162	0.20
U.2013E C7	0.2013E C7	0.162	0.20
U.3084E C7	0.3084E C7	0.162	0.20
U.7272E C7	0.7272E C7	0.162	0.20
U.1737E C7	0.1737E C7	0.162	0.20
U.8434E C6	0.8434E C6	0.162	0.20
U.3462E C6	0.3462E C6	0.162	0.20
U.2412E C6	0.2412E C6	0.162	0.20
U.1631E C6	0.1631E C6	0.162	0.20
U.1013E C5	0.1013E C5	0.162	0.20
U.7111E C5	0.7111E C5	0.162	0.20
U.2777E C5	0.2777E C5	0.162	0.20
U.1721E C5	0.1721E C5	0.162	0.20
U.8481E C5	0.8481E C5	0.162	0.20
U.1936E C5	0.1936E C5	0.162	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH PERCENT
U.1374E C5	0.1374E C5	0.1641E C7
U.4922E C7	0.4922E C7	0.1053E C7
U.2013E C7	0.2013E C7	0.124E C7
U.3084E C7	0.3084E C7	0.124E C7
U.7272E C7	0.7272E C7	0.126E C7
U.1737E C7	0.1737E C7	0.102E C7
U.8434E C6	0.8434E C6	0.059E C6
U.3462E C6	0.3462E C6	0.051E C6
U.2412E C6	0.2412E C6	0.051E C6
U.1631E C6	0.1631E C6	0.051E C6
U.1013E C5	0.1013E C5	0.051E C5
U.7111E C5	0.7111E C5	0.051E C5
U.2777E C5	0.2777E C5	0.051E C5
U.1721E C5	0.1721E C5	0.051E C5
U.8481E C5	0.8481E C5	0.051E C5
U.1936E C5	0.1936E C5	0.051E C5

THE ANNUAL YIELD IS 19.127 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4001E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.157E C7
 THE RATIO OF EGGS MATCHING TO EGGS SPANNED IS 0.5040E-05

YEAR 1944

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1742 C8	0.114	0.20
2	0.3742 C8	0.114	0.20
3	0.7742 C7	0.114	0.20
4	0.7742 C7	0.114	0.20
5	0.7742 C7	0.114	0.20
6	0.7742 C7	0.114	0.20
7	0.7742 C7	0.114	0.20
8	0.7742 C7	0.114	0.20
9	0.7742 C7	0.114	0.20
10	0.7742 C7	0.114	0.20
11	0.7742 C7	0.114	0.20
12	0.7742 C7	0.114	0.20
13	0.7742 C7	0.114	0.20
14	0.7742 C7	0.114	0.20
15	0.7742 C7	0.114	0.20
16	0.7742 C7	0.114	0.20
17	0.7742 C7	0.114	0.20
18	0.7742 C7	0.114	0.20
19	0.7742 C7	0.114	0.20

AGE GROUP	TOTAL BIOMASS LOST (EGG)	CONTRIBUTION TO CATCH PERCENT
1	0.3094 C7	0.154
2	0.4094 C7	0.154
3	0.4094 C7	0.154
4	0.4094 C7	0.154
5	0.4094 C7	0.154
6	0.4094 C7	0.154
7	0.4094 C7	0.154
8	0.4094 C7	0.154
9	0.4094 C7	0.154
10	0.4094 C7	0.154
11	0.4094 C7	0.154
12	0.4094 C7	0.154
13	0.4094 C7	0.154
14	0.4094 C7	0.154
15	0.4094 C7	0.154
16	0.4094 C7	0.154
17	0.4094 C7	0.154
18	0.4094 C7	0.154
19	0.4094 C7	0.154

THE ANNUAL YIELD IS 10.954 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4028E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5027E-05

YEAR 1945

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1742 C8	0.114	0.20
2	0.3742 C8	0.114	0.20
3	0.7742 C7	0.114	0.20
4	0.7742 C7	0.114	0.20
5	0.7742 C7	0.114	0.20
6	0.7742 C7	0.114	0.20
7	0.7742 C7	0.114	0.20
8	0.7742 C7	0.114	0.20
9	0.7742 C7	0.114	0.20
10	0.7742 C7	0.114	0.20
11	0.7742 C7	0.114	0.20
12	0.7742 C7	0.114	0.20
13	0.7742 C7	0.114	0.20
14	0.7742 C7	0.114	0.20
15	0.7742 C7	0.114	0.20
16	0.7742 C7	0.114	0.20
17	0.7742 C7	0.114	0.20
18	0.7742 C7	0.114	0.20
19	0.7742 C7	0.114	0.20

AGE GROUP	TOTAL BIOMASS LOST (EGG)	CONTRIBUTION TO CATCH PERCENT
1	0.3094 C7	0.154
2	0.4094 C7	0.154
3	0.4094 C7	0.154
4	0.4094 C7	0.154
5	0.4094 C7	0.154
6	0.4094 C7	0.154
7	0.4094 C7	0.154
8	0.4094 C7	0.154
9	0.4094 C7	0.154
10	0.4094 C7	0.154
11	0.4094 C7	0.154
12	0.4094 C7	0.154
13	0.4094 C7	0.154
14	0.4094 C7	0.154
15	0.4094 C7	0.154
16	0.4094 C7	0.154
17	0.4094 C7	0.154
18	0.4094 C7	0.154
19	0.4094 C7	0.154

THE ANNUAL YIELD IS 20.060 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4030E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5027E-05

YEAR 1946

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1742 C8	0.114	0.20
2	0.3742 C8	0.114	0.20
3	0.7742 C7	0.114	0.20
4	0.7742 C7	0.114	0.20
5	0.7742 C7	0.114	0.20
6	0.7742 C7	0.114	0.20
7	0.7742 C7	0.114	0.20
8	0.7742 C7	0.114	0.20
9	0.7742 C7	0.114	0.20
10	0.7742 C7	0.114	0.20
11	0.7742 C7	0.114	0.20
12	0.7742 C7	0.114	0.20
13	0.7742 C7	0.114	0.20
14	0.7742 C7	0.114	0.20
15	0.7742 C7	0.114	0.20
16	0.7742 C7	0.114	0.20
17	0.7742 C7	0.114	0.20
18	0.7742 C7	0.114	0.20
19	0.7742 C7	0.114	0.20

AGE GROUP	TOTAL BIOMASS LOST (EGG)	CONTRIBUTION TO CATCH PERCENT
1	0.3094 C7	0.154
2	0.4094 C7	0.154
3	0.4094 C7	0.154
4	0.4094 C7	0.154
5	0.4094 C7	0.154
6	0.4094 C7	0.154
7	0.4094 C7	0.154
8	0.4094 C7	0.154
9	0.4094 C7	0.154
10	0.4094 C7	0.154
11	0.4094 C7	0.154
12	0.4094 C7	0.154
13	0.4094 C7	0.154
14	0.4094 C7	0.154
15	0.4094 C7	0.154
16	0.4094 C7	0.154
17	0.4094 C7	0.154
18	0.4094 C7	0.154
19	0.4094 C7	0.154

THE ANNUAL YIELD IS 20.514 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4004E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5051E-05

YEAR 1997

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E C8	0.165	0.20
2	0.2434E C7	0.164	0.20
3	0.3624E C7	0.163	0.20
4	0.4814E C7	0.162	0.20
5	0.6004E C7	0.161	0.20
6	0.7194E C6	0.160	0.20
7	0.8384E C6	0.159	0.20
8	0.9574E C6	0.158	0.20
9	0.1076E C5	0.157	0.20
10	0.1176E C5	0.156	0.20
11	0.1276E C5	0.155	0.20
12	0.1376E C5	0.154	0.20
13	0.1476E C5	0.153	0.20
14	0.1576E C5	0.152	0.20
15	0.1676E C5	0.151	0.20
16	0.1776E C5	0.150	0.20

AGE GROUP	TOTAL BIOMASS LOST (Tg)	CONTRIBUTION TO CATCH PERCENT
1	0.1041E C7	0.146
2	0.2411E C7	0.297
3	0.4781E C7	0.594
4	0.7151E C7	0.891
5	0.9521E C7	1.188
6	0.1189E C6	0.165
7	0.1457E C6	0.202
8	0.1725E C6	0.239
9	0.1993E C6	0.276
10	0.2261E C6	0.313
11	0.2529E C6	0.350
12	0.2797E C6	0.387
13	0.3065E C6	0.424
14	0.3333E C6	0.461
15	0.3601E C6	0.498
16	0.3869E C6	0.535

THE ANNUAL YIELD IS 19.195 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.1084E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.1492E-05

YEAR 1998

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E C8	0.165	0.20
2	0.2434E C7	0.164	0.20
3	0.3624E C7	0.163	0.20
4	0.4814E C7	0.162	0.20
5	0.6004E C7	0.161	0.20
6	0.7194E C6	0.160	0.20
7	0.8384E C6	0.159	0.20
8	0.9574E C6	0.158	0.20
9	0.1076E C5	0.157	0.20
10	0.1176E C5	0.156	0.20
11	0.1276E C5	0.155	0.20
12	0.1376E C5	0.154	0.20
13	0.1476E C5	0.153	0.20
14	0.1576E C5	0.152	0.20
15	0.1676E C5	0.151	0.20
16	0.1776E C5	0.150	0.20

AGE GROUP	TOTAL BIOMASS LOST (Tg)	CONTRIBUTION TO CATCH PERCENT
1	0.1144E C7	0.142
2	0.2444E C7	0.297
3	0.4744E C7	0.594
4	0.7044E C7	0.891
5	0.9344E C7	1.188
6	0.1164E C6	0.165
7	0.1464E C6	0.202
8	0.1764E C6	0.239
9	0.2064E C6	0.276
10	0.2364E C6	0.313
11	0.2664E C6	0.350
12	0.2964E C6	0.387
13	0.3264E C6	0.424
14	0.3564E C6	0.461
15	0.3864E C6	0.498
16	0.4164E C6	0.535

THE ANNUAL YIELD IS 20.926 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.1084E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.160E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.1547E-05

YEAR 1999

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E C8	0.167	0.20
2	0.2434E C7	0.166	0.20
3	0.3624E C7	0.165	0.20
4	0.4814E C7	0.164	0.20
5	0.6004E C7	0.163	0.20
6	0.7194E C6	0.162	0.20
7	0.8384E C6	0.161	0.20
8	0.9574E C6	0.160	0.20
9	0.1076E C5	0.159	0.20
10	0.1176E C5	0.158	0.20
11	0.1276E C5	0.157	0.20
12	0.1376E C5	0.156	0.20
13	0.1476E C5	0.155	0.20
14	0.1576E C5	0.154	0.20
15	0.1676E C5	0.153	0.20
16	0.1776E C5	0.152	0.20

AGE GROUP	TOTAL BIOMASS LOST (Tg)	CONTRIBUTION TO CATCH PERCENT
1	0.2070E C7	0.134
2	0.4430E C7	0.289
3	0.6790E C7	0.538
4	0.9150E C7	0.787
5	0.1151E C6	0.100
6	0.1411E C6	0.125
7	0.1671E C6	0.150
8	0.1931E C6	0.175
9	0.2191E C6	0.200
10	0.2451E C6	0.225
11	0.2711E C6	0.250
12	0.2971E C6	0.275
13	0.3231E C6	0.300
14	0.3491E C6	0.325
15	0.3751E C6	0.350
16	0.4011E C6	0.375

THE ANNUAL YIELD IS 19.407 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.1051E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.1512E-05

AGE GROUP	SIZE	YEAR 2000	
		FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E 08	0.174	0.22
1	0.4627E 07	0.174	0.20
2	0.3142E 07	0.174	0.20
3	0.1190E 07	0.174	0.20
4	0.4170E 06	0.174	0.20
5	0.2592E 06	0.174	0.20
6	0.8071E 05	0.174	0.20
7	0.5562E 05	0.174	0.20
8	0.7020E 04	0.174	0.20
9	0.1135E 04	0.174	0.20
10	0.1011E 03	0.174	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH	PER FEMALE
0	0.2121E 07	0.1274E 01	0.22
1	0.1711E 07	0.1177E 01	0.156
2	0.4607E 07	0.2801E 01	0.193
3	0.3711E 07	0.2271E 01	0.103
4	0.2144E 07	0.1189E 01	0.097
5	0.1316E 07	0.8137E 00	0.057
6	0.8490E 06	0.3650E 00	0.114
7	0.3472E 06	0.4557E 00	0.032
8	0.1503E 06	0.4811E 00	0.007
9	0.4747E 05	0.6189E 00	0.002
10	0.4411E 05	0.4488E 00	0.001

THE ANNUAL YIELD IS 20.252 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3027E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1406 OF
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5123E-05

AGE GROUP	SIZE	YEAR 2001	
		FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E 08	0.174	0.20
1	0.4627E 07	0.174	0.20
2	0.3142E 07	0.174	0.20
3	0.1190E 07	0.174	0.20
4	0.4170E 06	0.174	0.20
5	0.2592E 06	0.174	0.20
6	0.8071E 05	0.174	0.20
7	0.5562E 05	0.174	0.20
8	0.7020E 04	0.174	0.20
9	0.1135E 04	0.174	0.20
10	0.1011E 03	0.174	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH	PER FEMALE
0	0.4422E 07	0.1871E 01	0.27
1	0.4877E 07	0.2921E 01	0.156
2	0.4681E 07	0.2664E 01	0.143
3	0.3233E 07	0.2171E 01	0.100
4	0.2131E 07	0.1414E 01	0.077
5	0.1162E 07	0.1057E 00	0.036
6	0.8560E 06	0.5127E 00	0.271
7	0.7043E 06	0.7117E 00	0.111
8	0.3673E 06	0.2201E 00	0.017
9	0.1347E 06	0.1577E 00	0.004
10	0.4731E 05	0.4677E 00	0.001
11	0.8124E 05	0.4277E 00	0.001

THE ANNUAL YIELD IS 18.762 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3055E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1576 OF
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5198E-05

AGE GROUP	SIZE	YEAR 2002	
		FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E 08	0.174	0.20
1	0.4627E 07	0.174	0.20
2	0.3142E 07	0.174	0.20
3	0.1190E 07	0.174	0.20
4	0.4170E 06	0.174	0.20
5	0.2592E 06	0.174	0.20
6	0.8071E 05	0.174	0.20
7	0.5562E 05	0.174	0.20
8	0.7020E 04	0.174	0.20
9	0.1135E 04	0.174	0.20
10	0.1011E 03	0.174	0.20

AGE GROUP	TOTAL BIOMASS LOST	CONTRIBUTION TO CATCH	PER FEMALE
0	0.3112E 07	0.1441E 01	0.241
1	0.3118E 07	0.1811E 01	0.124
2	0.4132E 07	0.2072E 01	0.144
3	0.3301E 07	0.1911E 01	0.126
4	0.2171E 07	0.1502E 01	0.037
5	0.1205E 07	0.1311E 00	0.036
6	0.8557E 06	0.4920E 00	0.037
7	0.7341E 06	0.7341E 00	0.218
8	0.3860E 06	0.2321E 00	0.005
9	0.1347E 06	0.1711E 00	0.005
10	0.4731E 05	0.4882E 00	0.003
11	0.8263E 05	0.4301E 00	0.001

THE ANNUAL YIELD IS 20.290 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.3061E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1598 OF
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.5073E-05

YEAR 2003

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
2	0.1274E C9	0.181	0.33
3	0.4481E C9	0.277	0.30
4	0.2657E C7	0.277	0.30
5	0.3477E C7	0.277	0.30
6	0.2037E C7	0.277	0.30
7	0.1709E C7	0.277	0.30
8	0.1221E C6	0.277	0.30
9	0.4165E C6	0.277	0.30
10	0.2611E C6	0.277	0.30
11	0.9218E C5	0.277	0.30
12	0.5516E C5	0.277	0.30
13	0.1404E C5	0.277	0.30
14	0.1404E C5	0.277	0.30
15	0.1108E C4	0.277	0.30
16	0.1041E C5	0.277	0.30

AGE GROUP	TOTAL BICASS LOST (EG)	CONTRIBUTION TO CATCH PERCENT
2	0.1033E C7	0.1375
3	0.4481E C7	0.2701
4	0.2654E C7	0.2717
5	0.3477E C7	0.2717
6	0.2037E C7	0.1407
7	0.1133E C7	0.1407
8	0.2381E C7	0.1087
9	0.1270E C6	0.1675
10	0.5701E C6	0.2127
11	0.3772E C6	0.2280
12	0.1404E C6	0.1818
13	0.1404E C6	0.8947
14	0.1404E C6	0.7088
15	0.5014E C5	0.2530
16	0.4481E C5	0.4111

THE ANNUAL YIELD IS 18.870 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4009E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1901 C7
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4652E-05

YEAR 2004

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
2	0.1274E C8	0.181	0.33
3	0.4481E C7	0.301	0.30
4	0.2657E C7	0.301	0.30
5	0.3477E C7	0.301	0.30
6	0.2037E C7	0.301	0.30
7	0.1709E C7	0.301	0.30
8	0.1221E C6	0.301	0.30
9	0.4165E C6	0.301	0.30
10	0.2611E C6	0.301	0.30
11	0.9218E C5	0.301	0.30
12	0.5516E C5	0.301	0.30
13	0.1404E C5	0.301	0.30
14	0.1404E C5	0.301	0.30
15	0.1108E C4	0.301	0.30
16	0.1041E C5	0.301	0.30

AGE GROUP	TOTAL BICASS LOST (EG)	CONTRIBUTION TO CATCH PERCENT
2	0.1033E C7	0.1375
3	0.4481E C7	0.2701
4	0.2654E C7	0.144
5	0.3477E C7	0.144
6	0.2037E C7	0.101
7	0.1133E C7	0.077
8	0.2381E C7	0.101
9	0.1270E C6	0.027
10	0.5701E C6	0.027
11	0.3772E C6	0.018
12	0.1404E C6	0.012
13	0.1404E C6	0.005
14	0.1404E C6	0.005
15	0.5014E C5	0.002
16	0.4481E C5	0.002

THE ANNUAL YIELD IS 19.343 THOUSAND METRIC TONS
 THE TOTAL NUMBER IN SPAWN FOR THE YEAR IS 0.4075E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.197E C7
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4969E-05

YEAR 2005

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
2	0.1374E C8	0.169	0.20
3	0.4501E C7	0.114	0.20
4	0.2674E C7	0.114	0.20
5	0.3477E C7	0.114	0.20
6	0.2037E C7	0.114	0.20
7	0.1709E C7	0.114	0.20
8	0.1221E C6	0.114	0.20
9	0.4165E C6	0.114	0.20
10	0.2611E C6	0.114	0.20
11	0.9218E C5	0.114	0.20
12	0.5516E C5	0.114	0.20
13	0.1404E C5	0.114	0.20
14	0.1404E C5	0.114	0.20
15	0.1108E C4	0.114	0.20
16	0.1041E C5	0.114	0.20

AGE GROUP	TOTAL BICASS LOST (EG)	CONTRIBUTION TO CATCH PERCENT
2	0.1094E C7	0.184E C7
3	0.4501E C7	0.3084E C7
4	0.2674E C7	0.120E C7
5	0.3477E C7	0.240E C7
6	0.2037E C7	0.2271E C7
7	0.1133E C7	0.2061E C7
8	0.2381E C7	0.1382E C7
9	0.1270E C6	0.1382E C6
10	0.5701E C6	0.5311E C6
11	0.3772E C6	0.383E C6
12	0.1404E C6	0.2377E C6
13	0.1404E C6	0.1511E C6
14	0.1404E C6	0.005
15	0.5014E C5	0.002
16	0.4481E C5	0.002

THE ANNUAL YIELD IS 20.237 THOUSAND METRIC TONS
 THE TOTAL NUMBER IN SPAWN FOR THE YEAR IS 0.4109E 13
 THE AVERAGE NUMBER IN EGGS PER FEMALE IS 0.1987 C7
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4929E-05

YEAR 2006

AGE GROUP	SEGS	FISHING MORTALITY	NATURAL MORTALITY
00	0.1371E 09	0.111	0.20
01	0.4249E 07	0.111	0.20
02	0.2721E 07	0.111	0.20
03	0.2035E 07	0.111	0.20
04	0.1572E 07	0.111	0.20
05	0.1207E 07	0.111	0.20
06	0.9237E 06	0.111	0.20
07	0.7072E 06	0.111	0.20
08	0.5447E 06	0.111	0.20
09	0.4197E 06	0.111	0.20
10	0.3237E 06	0.111	0.20
11	0.2497E 06	0.111	0.20
12	0.1927E 06	0.111	0.20
13	0.1477E 06	0.111	0.20
14	0.1127E 06	0.111	0.20
15	0.0857E 06	0.111	0.20
16	0.0657E 06	0.111	0.20
17	0.0507E 06	0.111	0.20
18	0.0387E 06	0.111	0.20
19	0.0297E 06	0.111	0.20
20	0.0227E 06	0.111	0.20
21	0.0177E 06	0.111	0.20
22	0.0137E 06	0.111	0.20
23	0.0107E 06	0.111	0.20
24	0.0087E 06	0.111	0.20
25	0.0067E 06	0.111	0.20
26	0.0057E 06	0.111	0.20
27	0.0047E 06	0.111	0.20
28	0.0037E 06	0.111	0.20
29	0.0037E 06	0.111	0.20
30	0.0037E 06	0.111	0.20
31	0.0037E 06	0.111	0.20
32	0.0037E 06	0.111	0.20
33	0.0037E 06	0.111	0.20
34	0.0037E 06	0.111	0.20
35	0.0037E 06	0.111	0.20
36	0.0037E 06	0.111	0.20
37	0.0037E 06	0.111	0.20
38	0.0037E 06	0.111	0.20
39	0.0037E 06	0.111	0.20
40	0.0037E 06	0.111	0.20
41	0.0037E 06	0.111	0.20
42	0.0037E 06	0.111	0.20
43	0.0037E 06	0.111	0.20
44	0.0037E 06	0.111	0.20
45	0.0037E 06	0.111	0.20
46	0.0037E 06	0.111	0.20
47	0.0037E 06	0.111	0.20
48	0.0037E 06	0.111	0.20
49	0.0037E 06	0.111	0.20
50	0.0037E 06	0.111	0.20

AGE GROUP TOTAL BIOMASS LOST CONTRIBUTION TO CATCH PERCENT

THE ANNUAL YIELD IS 20.780 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.40877E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNE IS 0.4854E-05

YEAR 2007

AGE GROUP	SEGS	FISHING MORTALITY	NATURAL MORTALITY
00	0.1371E 09	0.111	0.20
01	0.4249E 07	0.111	0.20
02	0.2721E 07	0.111	0.20
03	0.2035E 07	0.111	0.20
04	0.1572E 07	0.111	0.20
05	0.1207E 07	0.111	0.20
06	0.9237E 06	0.111	0.20
07	0.7072E 06	0.111	0.20
08	0.5447E 06	0.111	0.20
09	0.4197E 06	0.111	0.20
10	0.3237E 06	0.111	0.20
11	0.2497E 06	0.111	0.20
12	0.1927E 06	0.111	0.20
13	0.1477E 06	0.111	0.20
14	0.1127E 06	0.111	0.20
15	0.0857E 06	0.111	0.20
16	0.0657E 06	0.111	0.20
17	0.0507E 06	0.111	0.20
18	0.0387E 06	0.111	0.20
19	0.0297E 06	0.111	0.20
20	0.0227E 06	0.111	0.20
21	0.0177E 06	0.111	0.20
22	0.0137E 06	0.111	0.20
23	0.0107E 06	0.111	0.20
24	0.0087E 06	0.111	0.20
25	0.0067E 06	0.111	0.20
26	0.0057E 06	0.111	0.20
27	0.0047E 06	0.111	0.20
28	0.0037E 06	0.111	0.20
29	0.0037E 06	0.111	0.20
30	0.0037E 06	0.111	0.20
31	0.0037E 06	0.111	0.20
32	0.0037E 06	0.111	0.20
33	0.0037E 06	0.111	0.20
34	0.0037E 06	0.111	0.20
35	0.0037E 06	0.111	0.20
36	0.0037E 06	0.111	0.20
37	0.0037E 06	0.111	0.20
38	0.0037E 06	0.111	0.20
39	0.0037E 06	0.111	0.20
40	0.0037E 06	0.111	0.20
41	0.0037E 06	0.111	0.20
42	0.0037E 06	0.111	0.20
43	0.0037E 06	0.111	0.20
44	0.0037E 06	0.111	0.20
45	0.0037E 06	0.111	0.20
46	0.0037E 06	0.111	0.20
47	0.0037E 06	0.111	0.20
48	0.0037E 06	0.111	0.20
49	0.0037E 06	0.111	0.20
50	0.0037E 06	0.111	0.20

AGE GROUP TOTAL BIOMASS LOST CONTRIBUTION TO CATCH PERCENT

THE ANNUAL YIELD IS 19.750 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4046E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNE IS 0.4905E-05

YEAR 2008

AGE GROUP	SEGS	FISHING MORTALITY	NATURAL MORTALITY
00	0.1371E 09	0.111	0.20
01	0.4249E 07	0.111	0.20
02	0.2721E 07	0.111	0.20
03	0.2035E 07	0.111	0.20
04	0.1572E 07	0.111	0.20
05	0.1207E 07	0.111	0.20
06	0.9237E 06	0.111	0.20
07	0.7072E 06	0.111	0.20
08	0.5447E 06	0.111	0.20
09	0.4197E 06	0.111	0.20
10	0.3237E 06	0.111	0.20
11	0.2497E 06	0.111	0.20
12	0.1927E 06	0.111	0.20
13	0.1477E 06	0.111	0.20
14	0.1127E 06	0.111	0.20
15	0.0857E 06	0.111	0.20
16	0.0657E 06	0.111	0.20
17	0.0507E 06	0.111	0.20
18	0.0387E 06	0.111	0.20
19	0.0297E 06	0.111	0.20
20	0.0227E 06	0.111	0.20
21	0.0177E 06	0.111	0.20
22	0.0137E 06	0.111	0.20
23	0.0107E 06	0.111	0.20
24	0.0087E 06	0.111	0.20
25	0.0067E 06	0.111	0.20
26	0.0057E 06	0.111	0.20
27	0.0047E 06	0.111	0.20
28	0.0037E 06	0.111	0.20
29	0.0037E 06	0.111	0.20
30	0.0037E 06	0.111	0.20
31	0.0037E 06	0.111	0.20
32	0.0037E 06	0.111	0.20
33	0.0037E 06	0.111	0.20
34	0.0037E 06	0.111	0.20
35	0.0037E 06	0.111	0.20
36	0.0037E 06	0.111	0.20
37	0.0037E 06	0.111	0.20
38	0.0037E 06	0.111	0.20
39	0.0037E 06	0.111	0.20
40	0.0037E 06	0.111	0.20
41	0.0037E 06	0.111	0.20
42	0.0037E 06	0.111	0.20
43	0.0037E 06	0.111	0.20
44	0.0037E 06	0.111	0.20
45	0.0037E 06	0.111	0.20
46	0.0037E 06	0.111	0.20
47	0.0037E 06	0.111	0.20
48	0.0037E 06	0.111	0.20
49	0.0037E 06	0.111	0.20
50	0.0037E 06	0.111	0.20

AGE GROUP TOTAL BIOMASS LOST CONTRIBUTION TO CATCH PERCENT

THE ANNUAL YIELD IS 20.049 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4024E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNE IS 0.5077E-05

		YEAR 2009	
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E C8	0.177	0.70
1	0.4480E C7	0.370	0.70
2	0.3370E C7	0.400	0.70
3	0.2011E C7	0.370	0.70
4	0.1711E C7	0.300	0.70
5	0.2727E C6	0.370	0.70
6	0.4591E C6	0.300	0.70
7	0.9401E C5	0.300	0.70
8	0.5641E C5	0.300	0.70
9	0.3710E C5	0.300	0.70
10	0.2710E C5	0.300	0.70
11	0.1459E C4	0.300	0.70
12	0.1071E C4	0.300	0.70
AGE GROUP TOTAL BIOMASS LOST (MGT)			
0	0.3064E C7	0.1374E C7	0.171
1	0.4972E C7	0.3017E C7	0.154
2	0.4494E C7	0.2787E C7	0.142
3	0.1881E C7	0.2727E C7	0.100
4	0.1731E C7	0.1535E C7	0.078
5	0.2727E C6	0.4433E C6	0.301
6	0.4591E C6	0.2744E C6	0.078
7	0.9401E C5	0.2344E C5	0.012
8	0.5641E C5	0.2444E C5	0.005
9	0.3710E C5	0.5864E C5	0.003
10	0.2710E C5	0.3819E C5	0.002
11	0.0747E C4	0.4471E C4	0.001

THE ANNUAL YIELD IS 19.500 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4016E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.154E C7
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.5041E-05

		YEAR 2010	
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E C8	0.177	0.70
1	0.4480E C7	0.370	0.70
2	0.3370E C7	0.400	0.70
3	0.2011E C7	0.370	0.70
4	0.1711E C7	0.300	0.70
5	0.2727E C6	0.370	0.70
6	0.4591E C6	0.300	0.70
7	0.9401E C5	0.300	0.70
8	0.5641E C5	0.300	0.70
9	0.3710E C5	0.300	0.70
10	0.2710E C5	0.300	0.70
11	0.1459E C4	0.300	0.70
12	0.1071E C4	0.300	0.70
AGE GROUP TOTAL BIOMASS LOST (MGT)			
0	0.3064E C7	0.1374E C7	0.171
1	0.4972E C7	0.3017E C7	0.154
2	0.4494E C7	0.2837E C7	0.149
3	0.1881E C7	0.2727E C7	0.100
4	0.1731E C7	0.1535E C7	0.078
5	0.2727E C6	0.4433E C6	0.059
6	0.4591E C6	0.2744E C6	0.078
7	0.9401E C5	0.2344E C5	0.012
8	0.5641E C5	0.2444E C5	0.005
9	0.3710E C5	0.5864E C5	0.003
10	0.2710E C5	0.3819E C5	0.002
11	0.0747E C4	0.4471E C4	0.001

THE ANNUAL YIELD IS 19.776 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4024E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.1587E C7
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.5077E-05

		YEAR 2011	
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1374E C8	0.177	0.70
1	0.4480E C7	0.370	0.70
2	0.3370E C7	0.400	0.70
3	0.2011E C7	0.370	0.70
4	0.1711E C7	0.300	0.70
5	0.2727E C6	0.370	0.70
6	0.4591E C6	0.300	0.70
7	0.9401E C5	0.300	0.70
8	0.5641E C5	0.300	0.70
9	0.3710E C5	0.300	0.70
10	0.2710E C5	0.300	0.70
11	0.1459E C4	0.300	0.70
12	0.1071E C4	0.300	0.70
AGE GROUP TOTAL BIOMASS LOST (MGT)			
0	0.3064E C7	0.1374E C7	0.171
1	0.4972E C7	0.3017E C7	0.154
2	0.4494E C7	0.2847E C7	0.126
3	0.1881E C7	0.2727E C7	0.100
4	0.1731E C7	0.1535E C7	0.078
5	0.2727E C6	0.4433E C6	0.071
6	0.4591E C6	0.2744E C6	0.078
7	0.9401E C5	0.2344E C5	0.012
8	0.5641E C5	0.2444E C5	0.008
9	0.3710E C5	0.5864E C5	0.005
10	0.2710E C5	0.3819E C5	0.002
11	0.0747E C4	0.4471E C4	0.001

THE ANNUAL YIELD IS 19.730 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4037E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.148E C7
 THE RATIO OF EGGS HATCHING TO EGGS SPANNED IS 0.5018E-05

YEAR 2012

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	1.179E C9	0.124	0.20
1	0.313E C8	0.112	0.20
2	0.851E C7	0.112	0.20
3	0.343E C6	0.112	0.20
4	0.122E C5	0.112	0.20
5	0.429E C4	0.112	0.20
6	0.262E C3	0.112	0.20
7	0.452E C2	0.112	0.20
8	0.344E C1	0.112	0.20
9	0.159E C0	0.112	0.20
10	0.114E C0	0.112	0.20

AGE GROUP	TOTAL	BIO MASS LOST	CONTRIBUTION TO CATCH	PERCENT
0	0.3079E C7	0.1402E C7	0.0371	0.071
1	0.5017E C7	0.2058E C7	0.154	0.154
2	0.5025E C7	0.2061E C7	0.154	0.154
3	0.4091E C7	0.2654E C7	0.124	0.124
4	0.2790E C7	0.4082E C7	0.101	0.101
5	0.1844E C7	0.1124E C7	0.097	0.097
6	0.2127E C7	0.2920E C7	0.063	0.063
7	0.5025E C7	0.2061E C7	0.154	0.154
8	0.344E C1	0.1474E C1	0.003	0.003
9	0.159E C0	0.0747E C0	0.003	0.003
10	0.114E C0	0.0575E C0	0.003	0.003

THE ANNUAL YIELD IS 10.908 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4044E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.199E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4004E-05

YEAR 2013

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1379E C9	0.124	0.20
1	0.3271E C8	0.112	0.20
2	0.3421E C7	0.112	0.20
3	0.1732E C7	0.112	0.20
4	0.4181E C6	0.112	0.20
5	0.2471E C6	0.112	0.20
6	0.4332E C5	0.112	0.20
7	0.3271E C5	0.112	0.20
8	0.2471E C5	0.112	0.20
9	0.1379E C4	0.112	0.20
10	0.1044E C4	0.112	0.20

AGE GROUP	TOTAL	BIO MASS LOST	CONTRIBUTION TO CATCH	PERCENT
0	0.3179E C7	0.1402E C7	0.071	0.071
1	0.2010E C7	0.3057E C7	0.154	0.154
2	0.4044E C7	0.2061E C7	0.154	0.154
3	0.3303E C7	0.2014E C7	0.101	0.101
4	0.2247E C7	0.1397E C7	0.097	0.097
5	0.3021E C7	0.2041E C7	0.063	0.063
6	0.0491E C6	0.5491E C6	0.078	0.078
7	0.344E C6	0.244E C6	0.215	0.215
8	0.1805E C6	0.4784E C6	0.308	0.308
9	0.1805E C6	0.4784E C6	0.003	0.003
10	0.1794E C5	0.1794E C5	0.003	0.003

THE ANNUAL YIELD IS 10.898 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4044E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.199E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4004E-05

YEAR 2014

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1379E C9	0.105	0.20
1	0.3664E C8	0.105	0.20
2	0.3945E C7	0.105	0.20
3	0.2044E C7	0.105	0.20
4	0.1731E C7	0.105	0.20
5	0.4413E C6	0.105	0.20
6	0.1582E C6	0.105	0.20
7	0.4413E C5	0.105	0.20
8	0.3421E C5	0.105	0.20
9	0.2061E C5	0.105	0.20
10	0.1582E C4	0.105	0.20

AGE GROUP	TOTAL	BIO MASS LOST	CONTRIBUTION TO CATCH	PERCENT
0	0.2091E C7	0.1379E C7	0.071	0.071
1	0.4055E C7	0.2091E C7	0.154	0.154
2	0.4055E C7	0.2091E C7	0.154	0.154
3	0.4055E C7	0.2091E C7	0.124	0.124
4	0.3207E C7	0.1533E C7	0.101	0.101
5	0.1847E C7	0.1188E C7	0.097	0.097
6	0.1207E C6	0.2814E C6	0.063	0.063
7	0.4055E C6	0.2091E C6	0.018	0.018
8	0.2489E C6	0.1500E C6	0.003	0.003
9	0.1582E C6	0.9500E C6	0.003	0.003
10	0.1149E C5	0.1149E C5	0.003	0.003

THE ANNUAL YIELD IS 10.476 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4055E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.198E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPAWNED IS 0.4001E-05

YEAR 2015

AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
0	0.1101	0.1700	0.0000
1	0.1372	0.1700	0.0000
2	0.1700	0.1700	0.0000
3	0.2100	0.1700	0.0000
4	0.2500	0.1700	0.0000
5	0.2800	0.1700	0.0000
6	0.3100	0.1700	0.0000
7	0.3400	0.1700	0.0000
8	0.3700	0.1700	0.0000
9	0.4000	0.1700	0.0000
10	0.4300	0.1700	0.0000
11	0.4600	0.1700	0.0000
12	0.4900	0.1700	0.0000
13	0.5200	0.1700	0.0000
14	0.5500	0.1700	0.0000
15	0.5800	0.1700	0.0000
16	0.6100	0.1700	0.0000
17	0.6400	0.1700	0.0000
18	0.6700	0.1700	0.0000
19	0.7000	0.1700	0.0000
20	0.7300	0.1700	0.0000
21	0.7600	0.1700	0.0000
22	0.7900	0.1700	0.0000
23	0.8200	0.1700	0.0000
24	0.8500	0.1700	0.0000
25	0.8800	0.1700	0.0000
26	0.9100	0.1700	0.0000
27	0.9400	0.1700	0.0000
28	0.9700	0.1700	0.0000
29	1.0000	0.1700	0.0000
30	1.0300	0.1700	0.0000
31	1.0600	0.1700	0.0000
32	1.0900	0.1700	0.0000
33	1.1200	0.1700	0.0000
34	1.1500	0.1700	0.0000
35	1.1800	0.1700	0.0000
36	1.2100	0.1700	0.0000
37	1.2400	0.1700	0.0000
38	1.2700	0.1700	0.0000
39	1.3000	0.1700	0.0000
40	1.3300	0.1700	0.0000
41	1.3600	0.1700	0.0000
42	1.3900	0.1700	0.0000
43	1.4200	0.1700	0.0000
44	1.4500	0.1700	0.0000
45	1.4800	0.1700	0.0000
46	1.5100	0.1700	0.0000
47	1.5400	0.1700	0.0000
48	1.5700	0.1700	0.0000
49	1.6000	0.1700	0.0000
50	1.6300	0.1700	0.0000
51	1.6600	0.1700	0.0000
52	1.6900	0.1700	0.0000
53	1.7200	0.1700	0.0000
54	1.7500	0.1700	0.0000
55	1.7800	0.1700	0.0000
56	1.8100	0.1700	0.0000
57	1.8400	0.1700	0.0000
58	1.8700	0.1700	0.0000
59	1.9000	0.1700	0.0000
60	1.9300	0.1700	0.0000
61	1.9600	0.1700	0.0000
62	1.9900	0.1700	0.0000
63	2.0200	0.1700	0.0000
64	2.0500	0.1700	0.0000
65	2.0800	0.1700	0.0000
66	2.1100	0.1700	0.0000
67	2.1400	0.1700	0.0000
68	2.1700	0.1700	0.0000
69	2.2000	0.1700	0.0000
70	2.2300	0.1700	0.0000
71	2.2600	0.1700	0.0000
72	2.2900	0.1700	0.0000
73	2.3200	0.1700	0.0000
74	2.3500	0.1700	0.0000
75	2.3800	0.1700	0.0000
76	2.4100	0.1700	0.0000
77	2.4400	0.1700	0.0000
78	2.4700	0.1700	0.0000
79	2.5000	0.1700	0.0000
80	2.5300	0.1700	0.0000
81	2.5600	0.1700	0.0000
82	2.5900	0.1700	0.0000
83	2.6200	0.1700	0.0000
84	2.6500	0.1700	0.0000
85	2.6800	0.1700	0.0000
86	2.7100	0.1700	0.0000
87	2.7400	0.1700	0.0000
88	2.7700	0.1700	0.0000
89	2.8000	0.1700	0.0000
90	2.8300	0.1700	0.0000
91	2.8600	0.1700	0.0000
92	2.8900	0.1700	0.0000
93	2.9200	0.1700	0.0000
94	2.9500	0.1700	0.0000
95	2.9800	0.1700	0.0000
96	3.0100	0.1700	0.0000
97	3.0400	0.1700	0.0000
98	3.0700	0.1700	0.0000
99	3.1000	0.1700	0.0000
100	3.1300	0.1700	0.0000
101	3.1600	0.1700	0.0000
102	3.1900	0.1700	0.0000
103	3.2200	0.1700	0.0000
104	3.2500	0.1700	0.0000
105	3.2800	0.1700	0.0000
106	3.3100	0.1700	0.0000
107	3.3400	0.1700	0.0000
108	3.3700	0.1700	0.0000
109	3.4000	0.1700	0.0000
110	3.4300	0.1700	0.0000
111	3.4600	0.1700	0.0000
112	3.4900	0.1700	0.0000
113	3.5200	0.1700	0.0000
114	3.5500	0.1700	0.0000
115	3.5800	0.1700	0.0000
116	3.6100	0.1700	0.0000
117	3.6400	0.1700	0.0000
118	3.6700	0.1700	0.0000
119	3.7000	0.1700	0.0000
120	3.7300	0.1700	0.0000
121	3.7600	0.1700	0.0000
122	3.7900	0.1700	0.0000
123	3.8200	0.1700	0.0000
124	3.8500	0.1700	0.0000
125	3.8800	0.1700	0.0000
126	3.9100	0.1700	0.0000
127	3.9400	0.1700	0.0000
128	3.9700	0.1700	0.0000
129	4.0000	0.1700	0.0000
130	4.0300	0.1700	0.0000
131	4.0600	0.1700	0.0000
132	4.0900	0.1700	0.0000
133	4.1200	0.1700	0.0000
134	4.1500	0.1700	0.0000
135	4.1800	0.1700	0.0000
136	4.2100	0.1700	0.0000
137	4.2400	0.1700	0.0000
138	4.2700	0.1700	0.0000
139	4.3000	0.1700	0.0000
140	4.3300	0.1700	0.0000
141	4.3600	0.1700	0.0000
142	4.3900	0.1700	0.0000
143	4.4200	0.1700	0.0000
144	4.4500	0.1700	0.0000
145	4.4800	0.1700	0.0000
146	4.5100	0.1700	0.0000
147	4.5400	0.1700	0.0000
148	4.5700	0.1700	0.0000
149	4.6000	0.1700	0.0000
150	4.6300	0.1700	0.0000
151	4.6600	0.1700	0.0000
152	4.6900	0.1700	0.0000
153	4.7200	0.1700	0.0000
154	4.7500	0.1700	0.0000
155	4.7800	0.1700	0.0000
156	4.8100	0.1700	0.0000
157	4.8400	0.1700	0.0000
158	4.8700	0.1700	0.0000
159	4.9000	0.1700	0.0000
160	4.9300	0.1700	0.0000
161	4.9600	0.1700	0.0000
162	4.9900	0.1700	0.0000
163	5.0200	0.1700	0.0000
164	5.0500	0.1700	0.0000
165	5.0800	0.1700	0.0000
166	5.1100	0.1700	0.0000
167	5.1400	0.1700	0.0000
168	5.1700	0.1700	0.0000
169	5.2000	0.1700	0.0000
170	5.2300	0.1700	0.0000
171	5.2600	0.1700	0.0000
172	5.2900	0.1700	0.0000
173	5.3200	0.1700	0.0000
174	5.3500	0.1700	0.0000
175	5.3800	0.1700	0.0000
176	5.4100	0.1700	0.0000
177	5.4400	0.1700	0.0000
178	5.4700	0.1700	0.0000
179	5.5000	0.1700	0.0000
180	5.5300	0.1700	0.0000
181	5.5600	0.1700	0.0000
182	5.5900	0.1700	0.0000
183	5.6200	0.1700	0.0000
184	5.6500	0.1700	0.0000
185	5.6800	0.1700	0.0000
186	5.7100	0.1700	0.0000
187	5.7400	0.1700	0.0000
188	5.7700	0.1700	0.0000
189	5.8000	0.1700	0.0000
190	5.8300	0.1700	0.0000
191	5.8600	0.1700	0.0000
192	5.8900	0.1700	0.0000
193	5.9200	0.1700	0.0000
194	5.9500	0.1700	0.0000
195	5.9800	0.1700	0.0000
196	6.0100	0.1700	0.0000
197	6.0400	0.1700	0.0000
198	6.0700	0.1700	0.0000
199	6.1000	0.1700	0.0000
200	6.1300	0.1700	0.0000
201	6.1600	0.1700	0.0000
202	6.1900	0.1700	0.0000
203	6.2200	0.1700	0.0000
204	6.2500	0.1700	0.0000
205	6.2800	0.1700	0.0000
206	6.3100	0.1700	0.0000
207	6.3400	0.1700	0.0000
208	6.3700	0.1700	0.0000
209	6.4000	0.1700	0.0000
210	6.4300	0.1700	0.0000
211	6.4600	0.1700	0.0000
212	6.4900	0.1700	0.0000
213	6.5200	0.1700	0.0000
214	6.5500	0.1700	0.0000
215	6.5800	0.1700	0.0000
216	6.6100	0.1700	0.0000
217	6.6400	0.1700	0.0000
218	6.6700	0.1700	0.0000
219	6.7000	0.1700	0.0000
220	6.7300	0.1700	0.0000
221	6.7600	0.1700	0.0000
222	6.7900	0.1700	0.0000
223	6.8200	0.1700	0.0000
224	6.8500	0.1700	0.0000
225	6.8800	0.1700	0.0000
226	6.9100	0.1700	0.0000
227	6.9400	0.1700	0.0000
228	6.9700	0.1700	0.0000
229	7.0000	0.1700	0.0000
230	7.0300	0.1700	0.0000
231	7.0600	0.1700	0.0000
232	7.0900	0.1700	0.0000
233	7.1200	0.1700	0.0000
234	7.1500	0.1700	0.0000
235	7.1800	0.1700	0.0000
236	7.2100	0.1700	0.0000
237	7.2400	0.1700	0.0000
238	7.2700	0.1700	0.0000
239	7.3000	0.1700	0.0000
240	7.3300	0.1700	0.0000
241	7.3600	0.1700	0.0000
242	7.3900	0.1700	0.0000
243	7.4200	0.1700	0.0000
244	7.4500	0.1700	0.0000
245	7.4800	0.1700	0.0000
246	7.5100	0.1700	0.0000
247	7.5400	0.1700	0.0000
248	7.5700	0.1700	0.0000
249	7.6000	0.1700	0.0000
250	7.6300	0.1700	0.0000
251	7.6600	0.1700	0.0000
252	7.6900	0.1700	0.0000
253	7.7200	0.1700	0.0000
254	7.7500	0.1700	0.0000
255	7.7800	0.1700	0.0000
256	7.8100	0.1700	0.0000
257	7.8400	0.1700	0.0000
258	7.8700	0.1700	0.0000
259	7.9000	0.1700	0.0000
260	7.9300	0.1700	0.0000
261	7.9600	0.1700	0.0000
262	7.9900	0.1700	0.0000
263	8.0200	0.1700	0.0000
264	8.0500	0.1700	0.0000
265	8.0800	0.1700	0.0000
266	8.1100	0.1700	0.0000
267	8.1400	0.1700	0.0000
268	8.17		

YEAR 2018			
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E 08	0.110	0.20
2	0.4601E 07	0.110	0.20
3	0.5607E 07	0.110	0.20
4	0.3821E 07	0.110	0.20
5	0.2041E 07	0.110	0.20
6	0.1248E 07	0.110	0.20
7	0.1547E 06	0.110	0.20
8	0.4413E 06	0.110	0.20
9	0.2691E 06	0.110	0.20
10	0.1597E 06	0.110	0.20
11	0.9211E 05	0.110	0.20
12	0.5604E 05	0.110	0.20
13	0.3727E 05	0.110	0.20
14	0.2147E 05	0.110	0.20
15	0.1212E 05	0.110	0.20
16	0.7311E 04	0.110	0.20
17	0.1104E 04	0.110	0.20

AGE GROUP	TOTAL BICASS LOST	CONTRIBUTION TO CATCH
	(KG)	PERCENT
1	0.2010E 07	0.159
2	0.4964E 07	0.153
3	0.4972E 07	0.153
4	0.4424E 07	0.143
5	0.4220E 07	0.142
6	0.3785E 07	0.131
7	0.1192E 07	0.097
8	0.1192E 07	0.097
9	0.0241E 06	0.028
10	0.0604E 06	0.071
11	0.3907E 06	0.119
12	0.2491E 06	0.088
13	0.1889E 06	0.061
14	0.1040E 06	0.061
15	0.0607E 06	0.061
16	0.0372E 05	0.027
17	0.0072E 05	0.027

THE ANNUAL YIELD IS 10.715 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4045E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.159E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANMED IS 0.4098E-05

YEAR 2019			
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E 08	0.110	0.20
2	0.4601E 07	0.110	0.20
3	0.5607E 07	0.110	0.20
4	0.3821E 07	0.110	0.20
5	0.2041E 07	0.110	0.20
6	0.1248E 07	0.110	0.20
7	0.1547E 06	0.110	0.20
8	0.4413E 06	0.110	0.20
9	0.2691E 06	0.110	0.20
10	0.1597E 06	0.110	0.20
11	0.9211E 05	0.110	0.20
12	0.5604E 05	0.110	0.20
13	0.3727E 05	0.110	0.20
14	0.2147E 05	0.110	0.20
15	0.1212E 05	0.110	0.20
16	0.7311E 04	0.110	0.20
17	0.1104E 04	0.110	0.20

AGE GROUP	TOTAL BICASS LOST	CONTRIBUTION TO CATCH
	(KG)	PERCENT
1	0.2010E 07	0.171
2	0.4964E 07	0.144
3	0.4972E 07	0.142
4	0.4424E 07	0.142
5	0.4220E 07	0.142
6	0.3785E 07	0.138
7	0.1192E 07	0.091
8	0.1192E 07	0.091
9	0.0241E 06	0.028
10	0.0604E 06	0.071
11	0.3907E 06	0.119
12	0.2491E 06	0.088
13	0.1889E 06	0.061
14	0.1040E 06	0.061
15	0.0607E 06	0.061
16	0.0372E 05	0.027
17	0.0072E 05	0.027

THE ANNUAL YIELD IS 10.335 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4059E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.158E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANMED IS 0.4098E-05

YEAR 2020			
AGE GROUP	SIZE	FISHING MORTALITY	NATURAL MORTALITY
1	0.1374E 08	0.110	0.20
2	0.4601E 07	0.110	0.20
3	0.5607E 07	0.110	0.20
4	0.3821E 07	0.110	0.20
5	0.2041E 07	0.110	0.20
6	0.1248E 07	0.110	0.20
7	0.1547E 06	0.110	0.20
8	0.4413E 06	0.110	0.20
9	0.2691E 06	0.110	0.20
10	0.1597E 06	0.110	0.20
11	0.9211E 05	0.110	0.20
12	0.5604E 05	0.110	0.20
13	0.3727E 05	0.110	0.20
14	0.2147E 05	0.110	0.20
15	0.1212E 05	0.110	0.20
16	0.7311E 04	0.110	0.20
17	0.1104E 04	0.110	0.20

AGE GROUP	TOTAL BICASS LOST	CONTRIBUTION TO CATCH
	(KG)	PERCENT
1	0.2010E 07	0.170
2	0.5218E 07	0.153
3	0.5252E 07	0.154
4	0.4673E 07	0.143
5	0.4453E 07	0.143
6	0.3304E 07	0.131
7	0.1192E 07	0.097
8	0.1192E 07	0.097
9	0.0241E 06	0.028
10	0.0604E 06	0.071
11	0.3907E 06	0.119
12	0.2491E 06	0.088
13	0.1889E 06	0.061
14	0.1040E 06	0.061
15	0.0607E 06	0.061
16	0.0372E 05	0.027
17	0.0072E 05	0.027

THE ANNUAL YIELD IS 10.907 THOUSAND METRIC TONS
 THE TOTAL NUMBER OF SPAWN FOR THE YEAR IS 0.4082E 13
 THE AVERAGE NUMBER OF EGGS PER FEMALE IS 0.158E 07
 THE RATIO OF EGGS HATCHING TO EGGS SPANMED IS 0.4160E-05
 THE MINIMUM NUMBER OF PARTICLES IN THE SYSTEM AT ANY ONE TIME WAS 1794

THESE ARE THE LOSS RATES IN 10 ELEMENTS DUE TO TRANSPORT AND MORTALITY ON DAY 603, YEAR 1970

ELEMENT	INITIAL NUMBER	PERCENT TRANSPORT CUT	PERCENT DIED	RATIO
01	0.0	0.0	0.0	0.0
02	0.0	0.0	0.0	0.0
03	0.0	0.0	0.0	0.0
04	0.0	0.0	0.0	0.0
05	0.0	0.0	0.0	0.0
06	0.0	0.0	0.0	0.0
07	0.0	0.0	0.0	0.0
08	0.0	0.0	0.0	0.0
09	0.0	0.0	0.0	0.0
10	0.0	0.0	0.0	0.0
11	0.0	0.0	0.0	0.0
12	0.0	0.0	0.0	0.0
13	0.0	0.0	0.0	0.0
14	0.0	0.0	0.0	0.0
15	0.0	0.0	0.0	0.0
16	0.0	0.0	0.0	0.0
17	0.0	0.0	0.0	0.0
18	0.0	0.0	0.0	0.0
19	0.0	0.0	0.0	0.0
20	0.0	0.0	0.0	0.0
21	0.0	0.0	0.0	0.0
22	0.0	0.0	0.0	0.0
23	0.0	0.0	0.0	0.0
24	0.0	0.0	0.0	0.0
25	0.0	0.0	0.0	0.0
26	0.0	0.0	0.0	0.0
27	0.0	0.0	0.0	0.0
28	0.0	0.0	0.0	0.0
29	0.0	0.0	0.0	0.0
30	0.0	0.0	0.0	0.0
31	0.0	0.0	0.0	0.0
32	0.0	0.0	0.0	0.0
33	0.0	0.0	0.0	0.0
34	0.0	0.0	0.0	0.0
35	0.0	0.0	0.0	0.0
36	0.0	0.0	0.0	0.0
37	0.0	0.0	0.0	0.0
38	0.0	0.0	0.0	0.0
39	0.0	0.0	0.0	0.0
40	0.0	0.0	0.0	0.0
41	0.0	0.0	0.0	0.0
42	0.0	0.0	0.0	0.0
43	0.0	0.0	0.0	0.0
44	0.0	0.0	0.0	0.0
45	0.0	0.0	0.0	0.0
46	0.0	0.0	0.0	0.0
47	0.0	0.0	0.0	0.0
48	0.0	0.0	0.0	0.0
49	0.0	0.0	0.0	0.0
50	0.0	0.0	0.0	0.0
51	0.0	0.0	0.0	0.0
52	0.0	0.0	0.0	0.0
53	0.0	0.0	0.0	0.0
54	0.0	0.0	0.0	0.0
55	0.0	0.0	0.0	0.0
56	0.0	0.0	0.0	0.0
57	0.0	0.0	0.0	0.0
58	0.0	0.0	0.0	0.0
59	0.0	0.0	0.0	0.0
60	0.0	0.0	0.0	0.0
61	0.0	0.0	0.0	0.0
62	0.0	0.0	0.0	0.0
63	0.0	0.0	0.0	0.0
64	0.0	0.0	0.0	0.0
65	0.0	0.0	0.0	0.0
66	0.0	0.0	0.0	0.0
67	0.0	0.0	0.0	0.0
68	0.0	0.0	0.0	0.0
69	0.0	0.0	0.0	0.0
70	0.0	0.0	0.0	0.0
71	0.0	0.0	0.0	0.0
72	0.0	0.0	0.0	0.0
73	0.0	0.0	0.0	0.0
74	0.0	0.0	0.0	0.0
75	0.0	0.0	0.0	0.0
76	0.0	0.0	0.0	0.0
77	0.0	0.0	0.0	0.0
78	0.0	0.0	0.0	0.0
79	0.0	0.0	0.0	0.0
80	0.0	0.0	0.0	0.0
81	0.0	0.0	0.0	0.0
82	0.0	0.0	0.0	0.0
83	0.0	0.0	0.0	0.0
84	0.0	0.0	0.0	0.0
85	0.0	0.0	0.0	0.0
86	0.0	0.0	0.0	0.0
87	0.0	0.0	0.0	0.0
88	0.0	0.0	0.0	0.0
89	0.0	0.0	0.0	0.0
90	0.0	0.0	0.0	0.0
91	0.0	0.0	0.0	0.0
92	0.0	0.0	0.0	0.0
93	0.0	0.0	0.0	0.0
94	0.0	0.0	0.0	0.0
95	0.0	0.0	0.0	0.0
96	0.0	0.0	0.0	0.0
97	0.0	0.0	0.0	0.0
98	0.0	0.0	0.0	0.0
99	0.0	0.0	0.0	0.0
100	0.0	0.0	0.0	0.0
101	0.0	0.0	0.0	0.0
102	0.0	0.0	0.0	0.0
103	0.0	0.0	0.0	0.0
104	0.0	0.0	0.0	0.0
105	0.0	0.0	0.0	0.0
106	0.0	0.0	0.0	0.0
107	0.0	0.0	0.0	0.0
108	0.0	0.0	0.0	0.0
109	0.0	0.0	0.0	0.0
110	0.0	0.0	0.0	0.0
111	0.0	0.0	0.0	0.0
112	0.0	0.0	0.0	0.0
113	0.0	0.0	0.0	0.0
114	0.0	0.0	0.0	0.0
115	0.0	0.0	0.0	0.0
116	0.0	0.0	0.0	0.0
117	0.0	0.0	0.0	0.0
118	0.0	0.0	0.0	0.0
119	0.0	0.0	0.0	0.0
120	0.0	0.0	0.0	0.0
121	0.0	0.0	0.0	0.0
122	0.0	0.0	0.0	0.0
123	0.0	0.0	0.0	0.0
124	0.0	0.0	0.0	0.0
125	0.0	0.0	0.0	0.0
126	0.0	0.0	0.0	0.0
127	0.0	0.0	0.0	0.0
128	0.0	0.0	0.0	0.0
129	0.0	0.0	0.0	0.0
130	0.0	0.0	0.0	0.0
131	0.0	0.0	0.0	0.0
132	0.0	0.0	0.0	0.0
133	0.0	0.0	0.0	0.0
134	0.0	0.0	0.0	0.0
135	0.0	0.0	0.0	0.0
136	0.0	0.0	0.0	0.0
137	0.0	0.0	0.0	0.0
138	0.0	0.0	0.0	0.0
139	0.0	0.0	0.0	0.0
140	0.0	0.0	0.0	0.0
141	0.0	0.0	0.0	0.0
142	0.0	0.0	0.0	0.0
143	0.0	0.0	0.0	0.0
144	0.0	0.0	0.0	0.0
145	0.0	0.0	0.0	0.0
146	0.0	0.0	0.0	0.0
147	0.0	0.0	0.0	0.0
148	0.0	0.0	0.0	0.0
149	0.0	0.0	0.0	0.0
150	0.0	0.0	0.0	0.0
151	0.0	0.0	0.0	0.0
152	0.0	0.0	0.0	0.0
153	0.0	0.0	0.0	0.0
154	0.0	0.0	0.0	0.0
155	0.0	0.0	0.0	0.0
156	0.0	0.0	0.0	0.0
157	0.0	0.0	0.0	0.0
158	0.0	0.0	0.0	0.0
159	0.0	0.0	0.0	0.0
160	0.0	0.0	0.0	0.0
161	0.0	0.0	0.0	0.0
162	0.0	0.0	0.0	0.0
163	0.0	0.0	0.0	0.0
164	0.0	0.0	0.0	0.0

***** TERMINATION *****

12.5 Section 7 Appendix

12.5.1 Description of Computer Software

Computer Software for Qualitative/Quantitative IR Analysis

The laboratory is equipped with a Nova 3/12 Mini computer. The computer has 64K core memory, hard disk (10M byte) dual floppy disks (.3M byte each), 8 channel D/A board, 16 channel digital I/O board, A/D converter, foreground/background management system, two terminals and a digital plotter. It is interfaced to the Hewlett Packard GC/MS system and the Beckman 4260 Infrared Spectrometer. In addition, there is a Micro Nova, equipped with 28K core memory, dual floppy disks (.3M byte each) 8 channel D/A board, 16 channel digital I/O board, A/D converter, graphics terminal. It is interfaced to the P.E. gas chromatograph.

Extensive software was written for data collection and massage and is described in the following section.

1. Infrared Software

a) Program Descriptions:

i) IRBECK - this program collects the data from the Beckman 4260 Infrared spectrometer in 1 cm^{-1} increments and stores the data on file.

ii) SCALESUB - this program "separates" components from a mixture by subtracting the infrared spectrum of a particular component from the infrared spectrum of the mixture containing the component.

iii) ADDSPEC - this program adds two or more infrared spectra.

iv) ELASTASPEC - this program scales (expands or contracts) an infrared spectrum (in absorbance units).

v) HOW MUCH - this program determines the amount of a designated component in a sample.

Flow charts of the above programs are shown in Figures I-E-1 through 5.

b) Development of Data Acquisition Techniques

i) Determination of instrumental settings for measurement and computer storage of accurate spectra.

Although the measurement of high quality infrared spectra has always been essential for accurate sample analysis, it becomes even more critical for digitized infrared spectra. This requires the selection of instrumental conditions such that accurate data is transmitted to the computer during a scan. To choose these conditions, it is necessary to consider the magnitude of the signal reaching the detector. This is governed by the energy throughput of the sample.

IRBECK

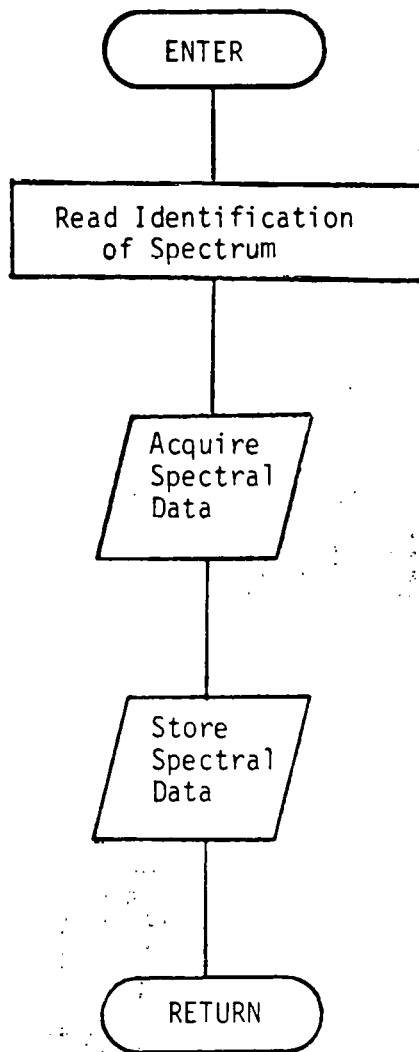


Figure I-E-1

SCALESUB

Figure 1-E-2.

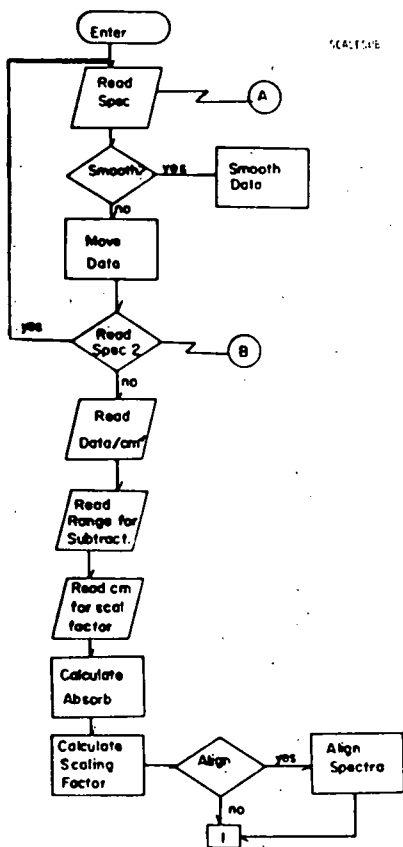


FIGURE 2b
SCALESUB

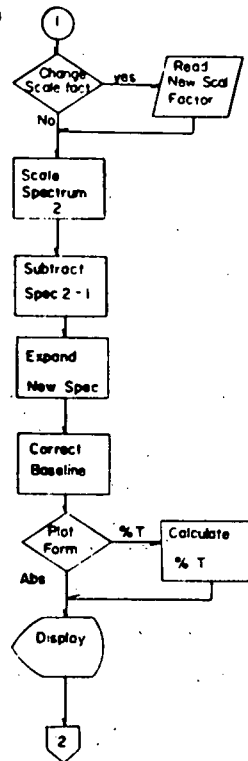


FIGURE 2c
SCALESUB

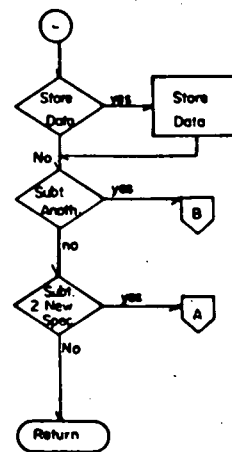
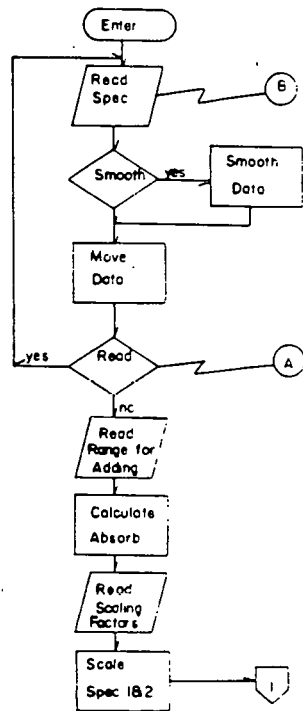
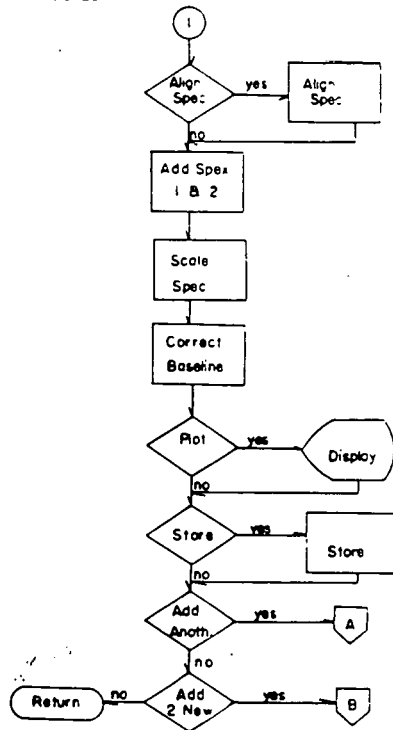


FIGURE 3a
ADDSPec



ADDSPec

FIGURE 3b
ADDSPec



ELASTASPEC

FIGURE 4a

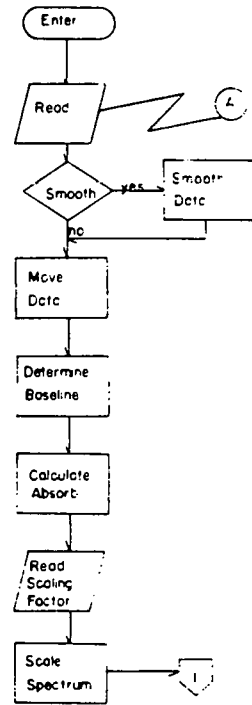
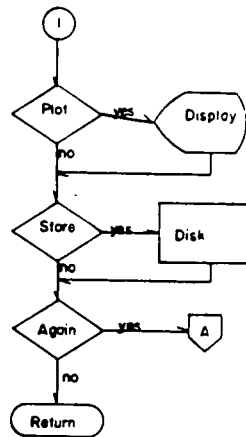


FIGURE 4b



HOWMUCH

FIGURE 5a
HOWMUCH

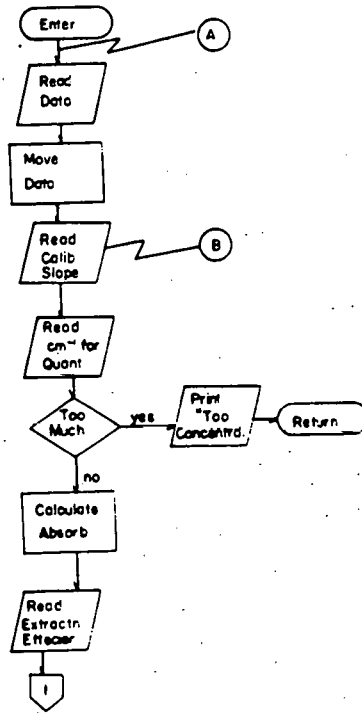
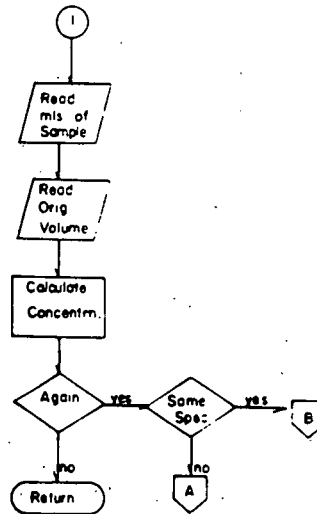


FIGURE 5b
HOWMUCH



For infrared analysis of the meso-tank samples, we are extracting water samples with CS₂ and transferring an aliquot of the sample to a sealed cell of 6 mm pathlength. To eliminate the absorptions due to the CS₂ in a spectrum, a second cell (also 6 mm pathlength) with pure CS₂ was placed in the reference beam of the instrument. The CS₂ then absorbs infrared energy from the sample and reference beams at its characteristic frequencies. The resultant spectrum was due to the absorption bands of the sample (solute). The absorption of energy from both beams by CS₂ greatly reduced the energy throughput of the sample.

To determine the proper instrumental parameters for measuring accurate spectra of samples in CS₂, a simple mixture of benzene-chloroform (1:1) was initially tested. In the region of interest between 1355 and 655 cm⁻¹, chloroform has two absorption bands (1210 and 755 cm⁻¹) and benzene has two absorption bands (1030 and 670 cm⁻¹).

The infrared spectrum of the benzene-chloroform mixture in CS₂ is shown in Figure I-E-6 (top). It shows the absorption bands of the mixture and the CS₂, because a compensating cell was not used in the reference beam.

The CS₂ absorbs totally between 880 and 830 cm⁻¹, resulting in a 50 cm⁻¹ region in which no energy reaches the detector. This divides the spectrum between 1355 and 655 cm⁻¹ into two "windows," wherein the absorptions due to the sample can be measured. The first window (1300-890 cm⁻¹) contains a CS₂ doublet centered at 1040 cm⁻¹. The second window (825-655 cm⁻¹) contains four relatively stronger bands due to the CS₂ (805, 785, 755, and 655 cm⁻¹).

The first optical window provides for a higher energy throughput because it contains the least intense CS₂ bands. Considering this window first, instrument settings were chosen for this available energy. Instrument gain was chosen for this region according to instrument specifications. Slits were set at .3 mm at 3000 cm⁻¹. The third important parameter, scan speed, was chosen by repeated scans of this sample at varying speeds and speed suppressions and by storing these data on the computer.

Tracking error is introduced into the measurement if the scan is not slow enough. To determine at which speed the tracking error was eliminated in the measurement, it was assumed that a spectrum measured accurately at, e.g., 300 cm⁻¹/min. with a speed suppression of 2, would be identical to a spectrum of the same sample measured accurately at 300 cm⁻¹/min. with a speed suppression of 1. Subtraction of these two spectra should give a horizontal (straight) line. Any deviation from a straight line is a gauge of the inaccuracy of spectral measurement in either or both spectra.

Figure I-E-6 (bottom) shows the compensated infrared spectrum of the mixture of CS₂. This spectrum was scanned in the 1300-1000 cm region at speeds of 1000, 600, 300, and 150 cm⁻¹/min. At each speed, the speed

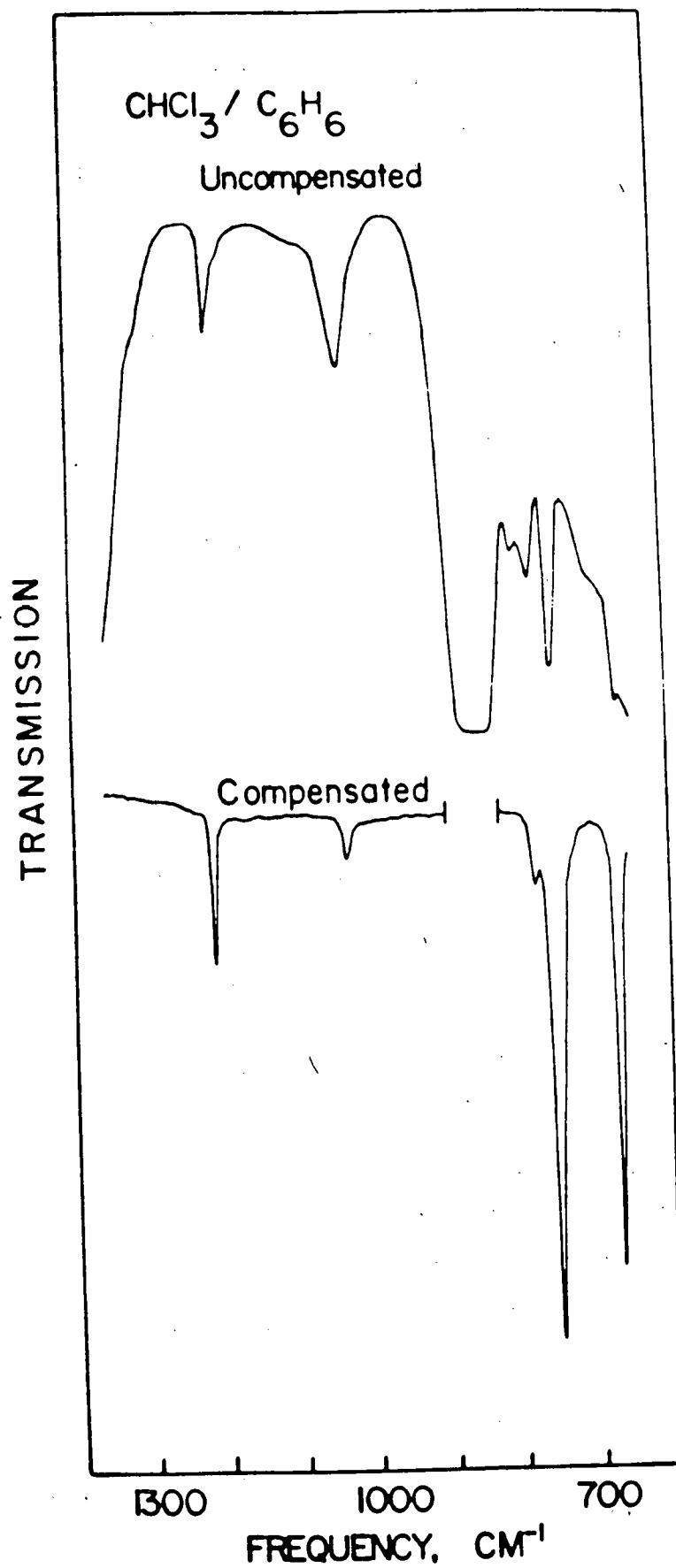


Figure I-E-6.

suppression was also varied from 3 to 0, yielding three spectra at each speed for a total of 12 spectra. At each speed, subtractions were performed between the spectra measured at the various speed suppressions.

Figure I-E-7 shows the results of these subtractions. It can be seen that at slower speeds and higher speed suppressions, deviation from a straight line plot is minimized. There is still some difference evidenced at 150 $\text{cm}^{-1}/\text{min.}$, speed suppression 3-2; thus, it was decided to measure additional spectra at 150 $\text{cm}^{-1}/\text{min.}$ with a speed suppression of 4 and at 50 $\text{cm}^{-1}/\text{min.}$ with a speed suppression 1 and 0. Figure I-E-8 shows the results of subtractions of these additional spectra. It can be seen that by the subtraction of the spectrum measured at 150 $\text{cm}^{-1}/\text{min.}$ with a speed suppression of 3 from speed suppression of 4, there is a slight deviation. By slowing the scan down to 50 $\text{cm}^{-1}/\text{min.}$ and subtracting speed suppression 0 from speed suppression 1, a straight line was obtained.

To determine whether or not the spectrum measured at 150 $\text{cm}^{-1}/\text{min.}$ with a speed suppression of 4 was measured with acceptable accuracy, it was then subtracted from the spectrum measured at 50 cm^{-1} with a speed suppression of 1. As can be seen in Figure I-E-8, a relatively straight line was also obtained, indicating that within this "window," a spectrum would be accurately measured at a speed 150 $\text{cm}^{-1}/\text{min.}$ with a speed suppression of 4.

Moving to the second "window" (825-655 cm^{-1}), we find a different energy situation. CS_2 has more intense bands here, resulting in a lower energy throughput than in the first situation. This requires a slight increase in instrument gain and the determination of proper scan speed. From the results already obtained, we know that it is not possible to scan faster than 150 $\text{cm}^{-1}/\text{min.}$ Therefore, spectra of the mixture were measured at 150 $\text{cm}^{-1}/\text{min.}$ with speed suppression varying from 4 to 1, yielding 4 spectra.

Subtractions of these spectra from one another are shown in Figure I-E-9. The subtraction of a spectrum at speed suppression 3 from the one measured at speed suppression 4 gives slight deviations. The spectrum of the mixture between 1355 and 655 cm^{-1} was, therefore, measured at 150 $\text{cm}^{-1}/\text{min.}$ with a speed suppression of 4.

The infrared spectra of the components were individually measured in the same region, under the same conditions. Figure I-E-10 shows the spectra of the benzene and chloroform. Beneath the benzene is the spectrum resulting from the subtraction of chloroform from the mixture, yielding benzene. Beneath the spectrum of the chloroform is the spectrum resulting from the subtraction of benzene from the mixture, yielding chloroform.

It can be seen that both spectra resulting from these subtractions vary slightly from the spectra of the corresponding pure compound in the 825-655 cm^{-1} region. To determine the stability of the sample in the infrared beam for this region, five repetitive infrared scans of the mixture were made. In each case, the sample remained in the infrared beam for 20 minutes.

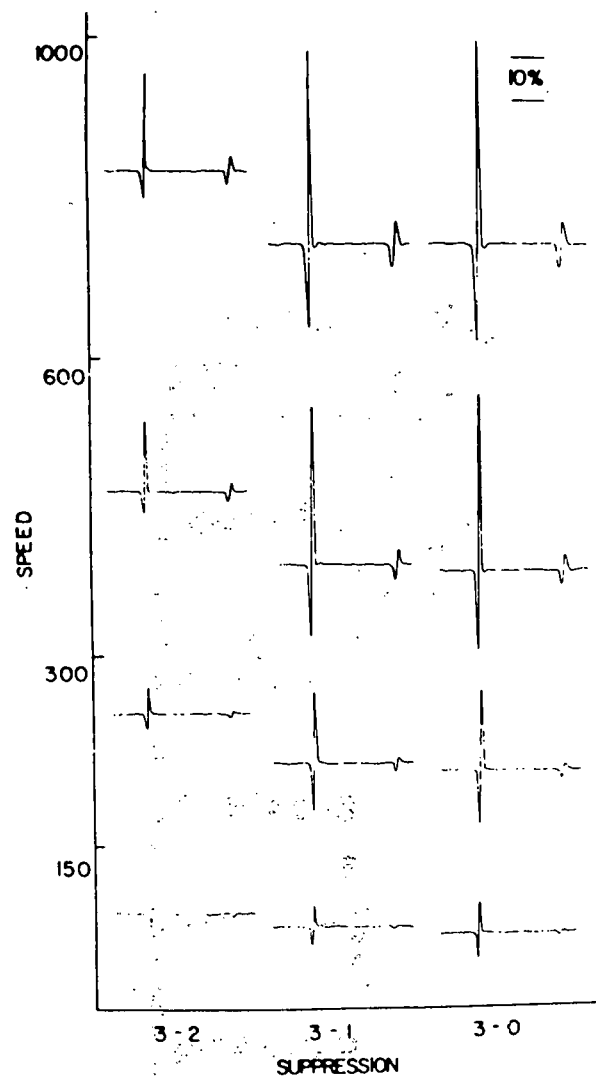


Figure 1-E-7.

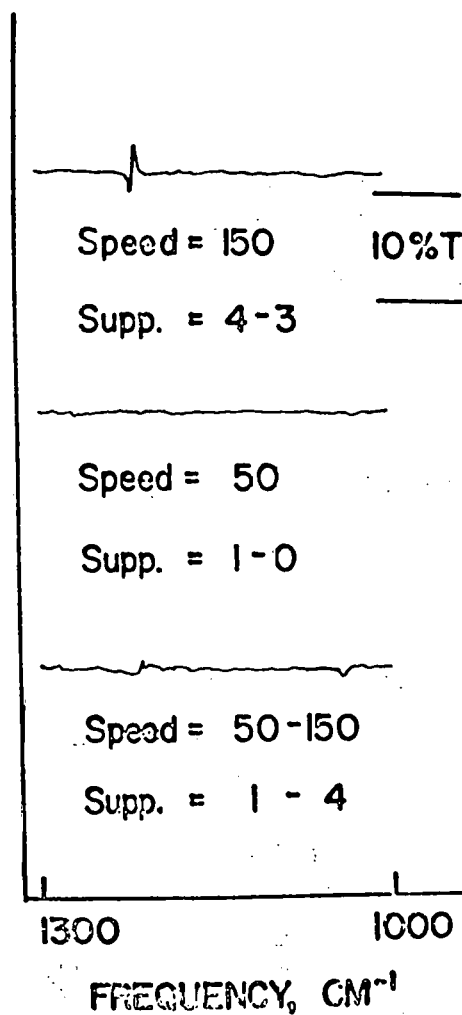


Figure 1-E-8.

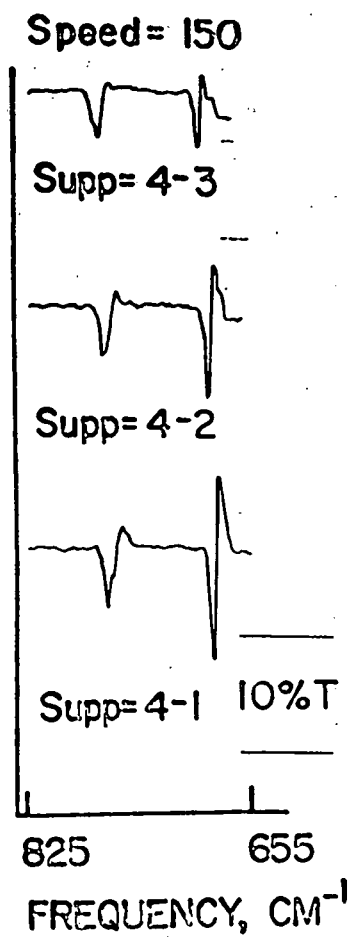


Figure I-E-9.

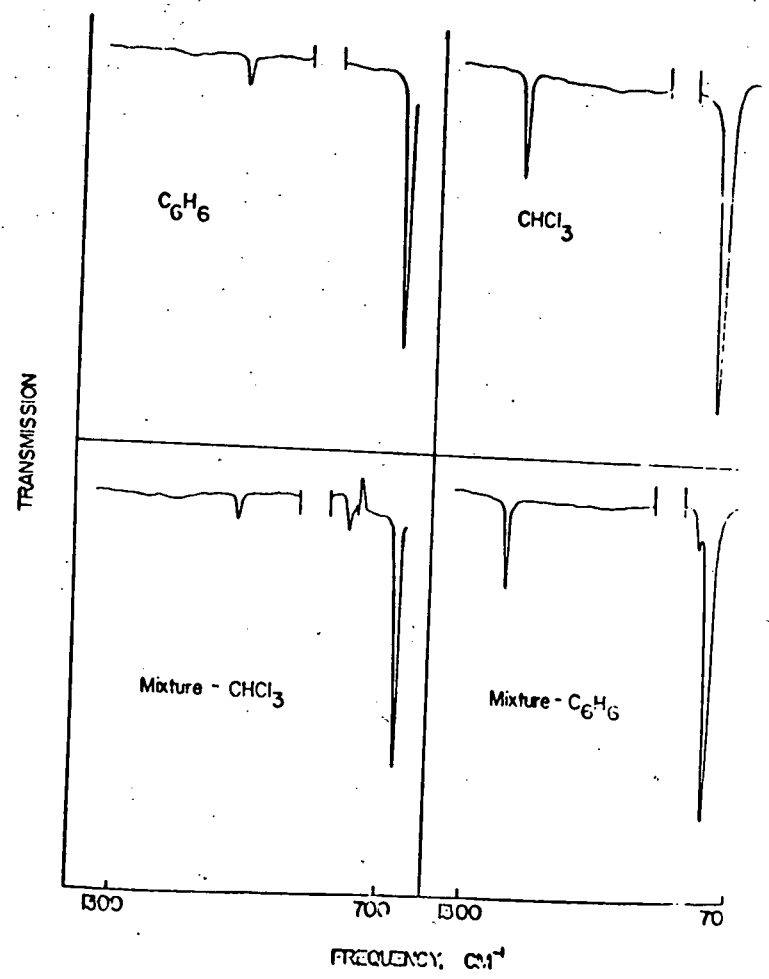


Figure I-E-10.

Figure I-E-11 shows the results of subtracting the fifth scan from the first scan. As can be seen, neither the mixture nor either of the individual components yield a straight line, indicating an instability in the infrared spectrum of each sample with time. This accounts for the poor subtractions in the 825-655 cm^{-1} region.

Considering the instability of this mixture in the fingerprint region, it was decided to move to another sample type. A mixture of dibutyl, diisobutyl, and dioctyl phthalate were placed into CS_2 solution. Phthalates are a common contaminant in organic extracts from sea water and the sources of phthalates are numerous. They can occur from leaching of PVC pipes in the tanks. We have detected phthalates in some "pure" lots of CS_2 . Certain phthalates are also naturally present in sea water. It is necessary to separate these contaminants from the hydrocarbon extracts before sample analysis. Several infrared scans of the phthalate mixture were, therefore, measured and the sample was found to be relatively stable in the infrared beam.

Figure I-E-12 shows the uncompensated and compensated infrared spectrum of the phthalate mixture in CS_2 . As can be seen, this sample has many more absorption bands in this infrared region than did the previous mixture. Therefore, it would be expected that the rate of scan necessary for measurement of an accurate spectrum would be 150 $\text{cm}^{-1}/\text{min}$. with speed suppression of 4, or possibly slower. It would be very desirable to be able to increase the scan rate, and one way to allow for a faster scan without sacrificing spectral accuracy might be to increase the slit-width. This would increase energy throughput to the detector. There is, however, a loss of spectral resolution with increase in slit-width.

Figure I-E-13 shows the infrared spectra of the phthalate mixture measured with the slit-width set for .3mm and for .45 mm at 3000 cm^{-1} . The spectra show that with a 50% increase in slit-width, resolution is not sacrificed to any appreciable degree.

Infrared spectra of the mixture were then measured at 150 $\text{cm}^{-1}/\text{min}$., varying the speed suppression from 4 to 0, yielding five spectra. Subtraction of the spectrum measured at speed suppression 0 from that measured at speed suppression 4 yielding the straight line in Figure I-E-13. Thus by opening the slits to .45 mm at 3000 cm^{-1} , we are able to scan approximately twice as fast as a slit-width of .3mm.

The computer programs were next tested on separation of phthalates from hydrocarbon samples. The top spectrum of Figure I-E-14 is that of a mixture of Kuwait oil and phthalates in CS_2 . The middle spectrum is the result of subtracting a spectrum of the phthalate spectrum from the top spectrum, yielding a spectrum of oil. The bottom spectrum is of the pure oil in CS_2 .

The two lower spectra are almost identical indicating a successful separation of phthalates from the mixture.

The subtraction program is also directly applicable to the separation of dispersant from a mixture of oil and dispersant. The meso-tank experiments were designed so that the fate of oil in water and that of oil carried into the water column by a dispersant were monitored under

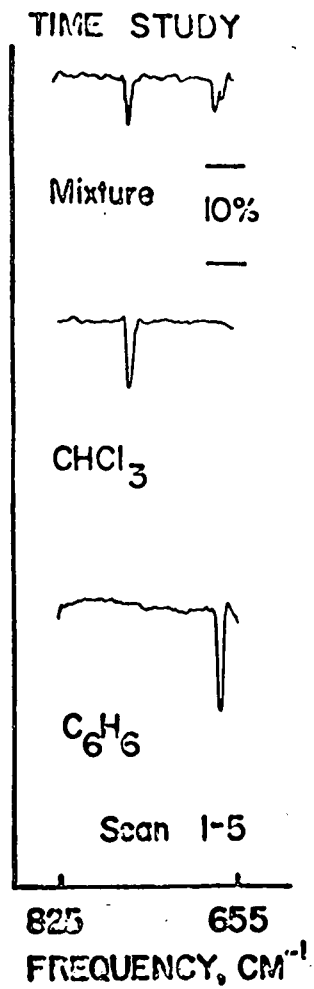


Figure I-E-11.

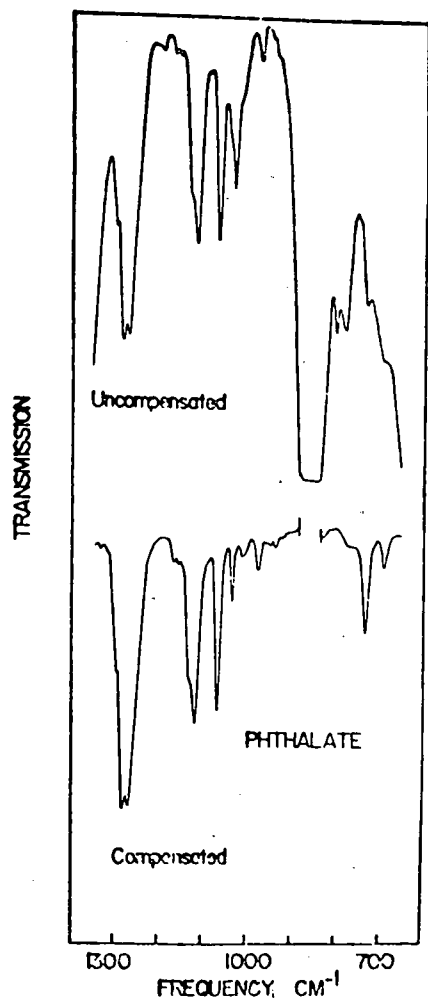


Figure I-E-12.

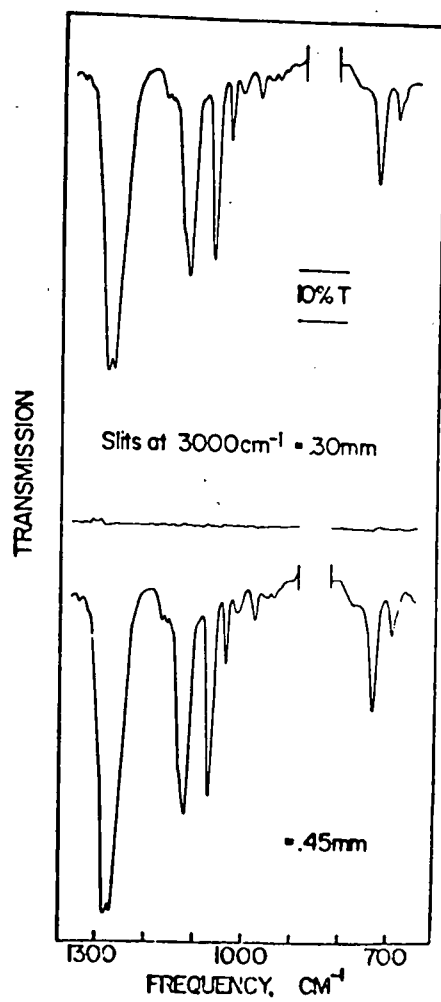


Figure I-E-13.

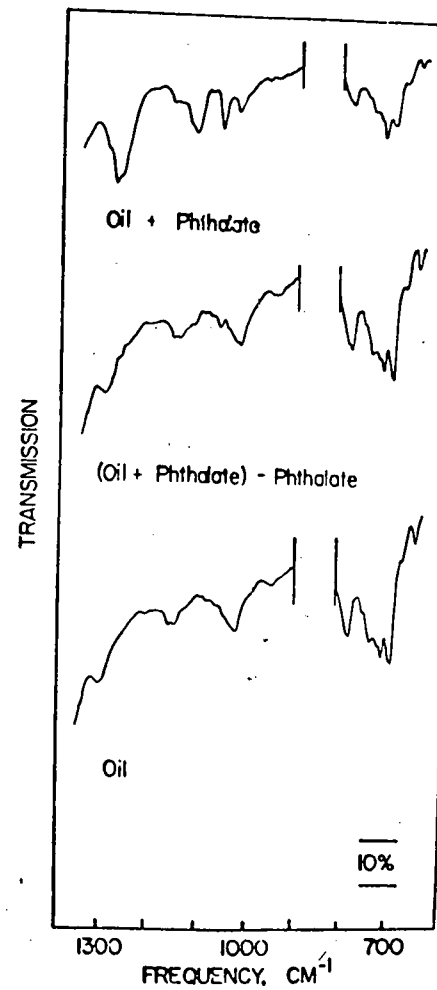


Figure I-E-14.

identical conditions. Oil was "spilled" into one tank while oil and dispersant were spilled into the other tank. Water samples of both tanks were collected at varying depths and the hydrocarbons were then extracted with CS_2 .

To determine the types and amounts of petroleum hydrocarbons present in the oil/dispersant tank samples, it is necessary to separate the oil from the dispersant. Like the oil, the dispersant is also a complex mixture of hydrocarbons which has a very strong and complex infrared spectrum.

Figure I-E-15 shows the infrared spectra of oil on CS_2 as well as dispersant in CS_2 in the $4000-650\text{ cm}^{-1}$ region. As can be seen, the dispersant has hydrocarbon bands between 3000 and 2900 cm^{-1} which overlap with the hydrocarbon bands due to the Kuwait oil. The 2930 cm^{-1} band is used for quantitative analysis of petroleum hydrocarbons. Therefore, it is necessary to eliminate the overlapping dispersant band in this region. Looking at the fingerprint region ($1355-655\text{ cm}^{-1}$), it can be seen that the dispersant also has relatively intense bands which overlap with the bands of the oil. To perform qualitative analysis of the petroleum, the absorption bands due to the dispersant must be eliminated as well.

Since dispersants and petroleum are both complex mixtures of hydrocarbons, chemical separation of these two mixtures is extremely difficult, if not altogether impossible.

To determine the feasibility of separating these two mixtures spectrally, a mixture of Kuwait oil and dispersant was placed in CS_2 . The top spectrum in Figure I-E-16 is of the mixture. The concentration of the oil and the dispersant were both known. A CS_2 solution of a known amount of dispersant was also prepared.

The middle spectrum is the result of the subtraction of the spectrum of the dispersant from that of the oil/dispersant mixture. The bottom spectrum is of Kuwait oil. Comparison of the lower two spectra shows them to be almost identical, indicating a successful separation of oil and dispersant. The fingerprint of the oil is free from interfering dispersant bands and can be used for qualitative analysis.

When subtracting the dispersant from the mixture, a factor is calculated and this factor is used to scale the spectrum of the pure dispersant so that the intensity of the dispersant bands in the pure solution match that of the dispersant bands in the mixture. The scaling factor should provide a means to determine the amount of a component in a mixture.

The concentration of dispersant in CS_2 was known. By multiplying the scaling factor obtained from the subtraction in Figure I-E-16 by the known concentration, a concentration of $540-545\text{ ppm}$ was obtained. The concentration of the dispersant in the mixture was known to be 542 ppm . Knowing the concentration of dispersant in the mixture, we can now determine the amount of hydrocarbon due to petroleum.

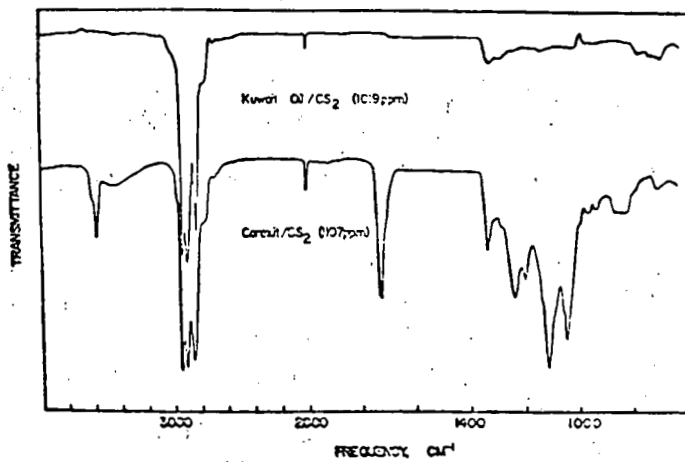


Figure I-E-15. Infrared Spectra of a Known Concentration of Kuwait Oil in CS₂, and a Known Concentration of Corexit in CS₂

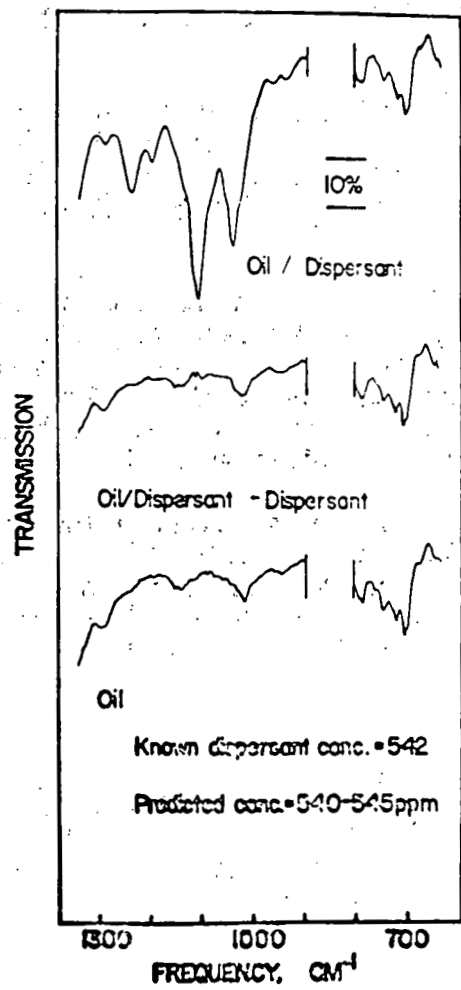


Figure I-E-16.

Solutions of pure compounds in CS₂ were used for this series of tests of the computer programs. However, samples from the tank experiments are CS₂ extracts of the oil, oil/dispersant and dispersant from sea water. To determine how these samples differ from CS₂ solutions of the neat compounds, laboratory experiments were conducted in which oil, oil/dispersant and dispersant were "spilled" into large containers of sea water. One liter samples of these "spills" were then extracted with CS₂, along with a control.

The top spectrum in Figure I-E-17 is of the neat oil in CS₂. The spectrum of the control was subtracted from that of the CS₂ extract of the oil from the water. Differences in the relative intensities of the bands can be seen between corresponding bands in each spectrum.

The top spectrum in Figure I-E-18 is that of the CS₂ extract of the oil/dispersant mixture from water, minus its control. The middle spectrum is of the CS₂ extract of the dispersant from water minus control. The bottom spectrum is the result of the subtraction of the middle spectrum from the top spectrum, yielding a spectrum of the oil carried into the water by the dispersant.

In Figure I-E-19, the top spectrum is the result of the subtraction shown in Figure I-E-18, i.e., the oil carried into the water by the dispersant. The middle spectrum is the result of the subtraction in Figure I-E-17, i.e., the oil in water. The bottom spectrum is of neat oil in CS₂. The three spectra are obviously different in contours and relative intensities, indicating a difference in chemical composition between samples.

2) GC Software and GC/MS Software

Computer programs for massage of the GC data were developed by this laboratory.

a) Program Descriptions

i) GCPE - can acquire GC data for any length of time. From the user input information, initial temperature, final temperature, rate and number of minutes, the program determines how many times to acquire 3600 consecutive data points in a 'do-loop.' The data acquisition rate is three points per second so a forty-five minute run will have 8100 data points or will need to cycle the 'do-loop' twice ($2 \times 3600 = 7200$) and acquire the last 900 points (remainder) outside of the 'do-loop.' Along with storing the data and data name, the initial temperature, rate and number of minutes are also stored (Figure I-E-20).

ii) SMOTH9 - this 9 point smoothing routine will open any data file created by GCPE and display the smoothed chromatogram on a Houston Instrument Complot. This program is really the reverse of GCPE in that it generates the smoothed data in 3600 data point arrays and then generates the remainder of the data points. A graphical example of the smoothing is shown in Figure I-E-21. 1 through I-4 cannot be calculated due to the nature of the general smoothing formula.

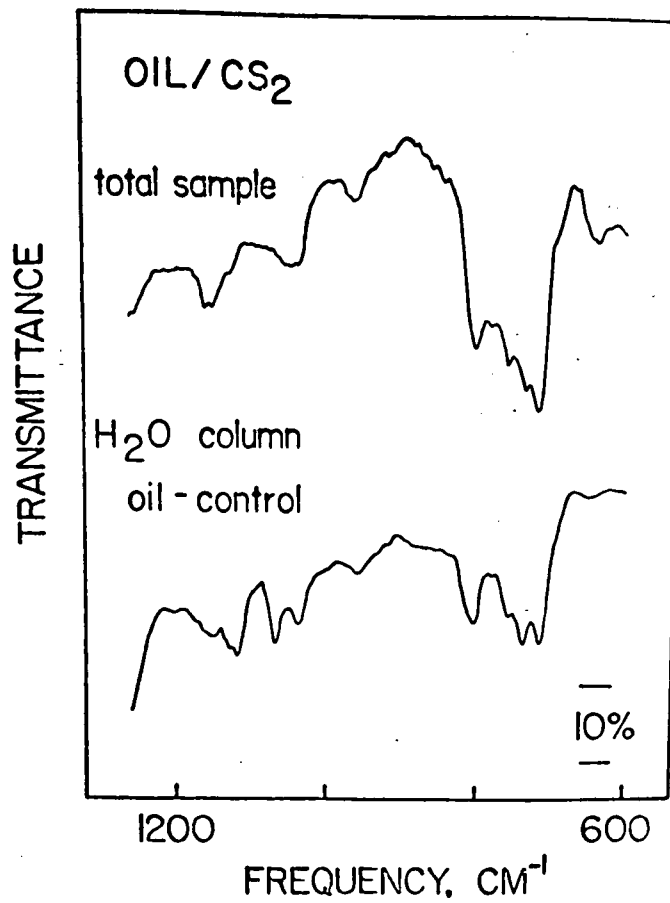


Figure I-E-17.

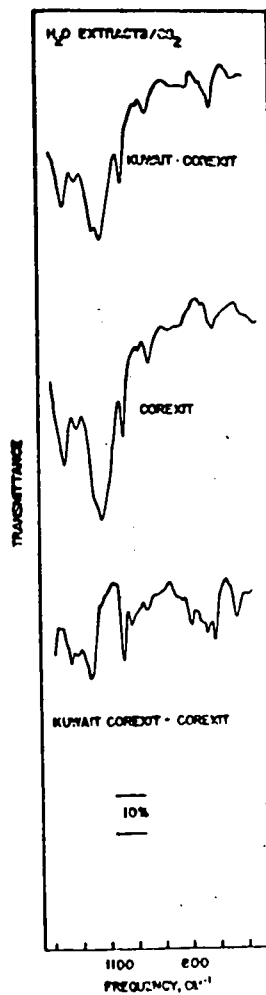


Figure I-E-18.

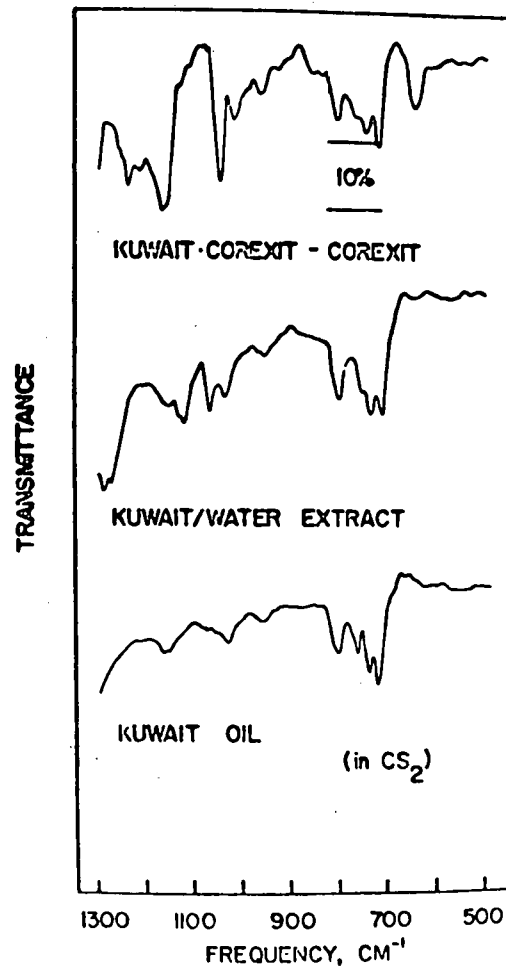


Figure I-E-19.

GCPE
(collects data)

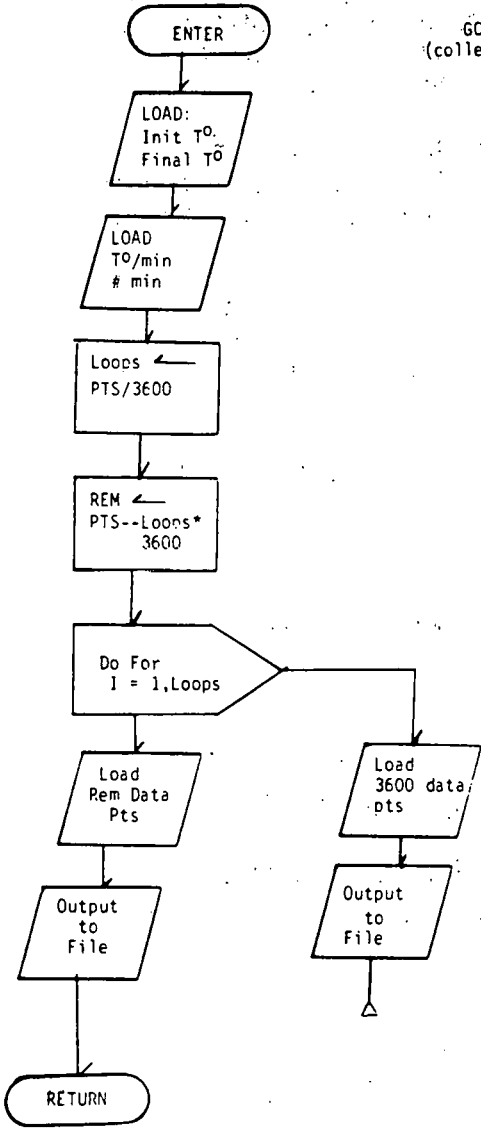


Figure I-E-20

SMOTH 9
(Plots Data)

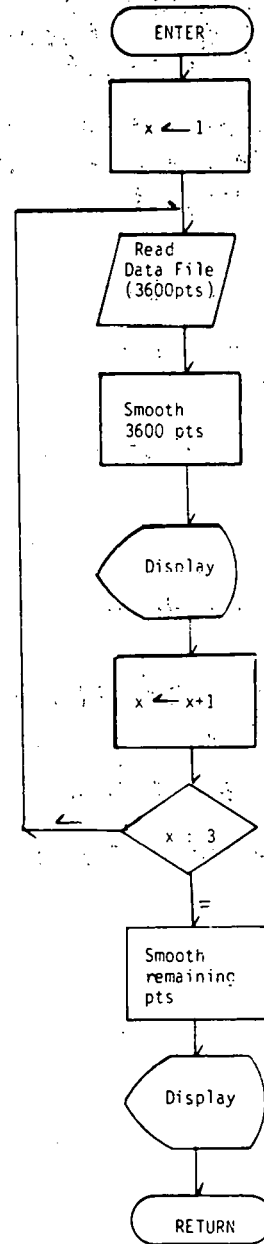


Figure I-E-21

(iii) MSPEC.FR - scans and acquires data from the GC/MS system. Stores data on disk for subsequent data processing and display. Uses subroutine GOMS.SR. Outputs a 0 to -10 VDC staircase voltage ramp in 400 steps. At every step (corresponding to one amu, 400 amu full scan) a signal is taken off the electron multiplier via the Nova ADC.

TOTION.FR - plots out on the plotter a reconstructed gas chromatogram for the entire analysis. This is called a total ion plot. For each reconstructed GC peak, a mass spectrum may be displayed via program MSPLT.FR or MASSPLOT.FR.

MSPLT.FR - plot out individual mass spectra on CRT.

MASSPLOT.FR - plot out individual mass spectra on plotter, same as flow diagram for MSPLT.FR.

MSSERCH.FR - determines if a particular mass is present in an analysis.

References

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2. D. Goldfarb & C.W. Brown, Appl. Spectrosc. 33,126 (1979).
3. P.F. Lynch & M.M. Brady, Anal. Chem. 50, 1520 (1978).
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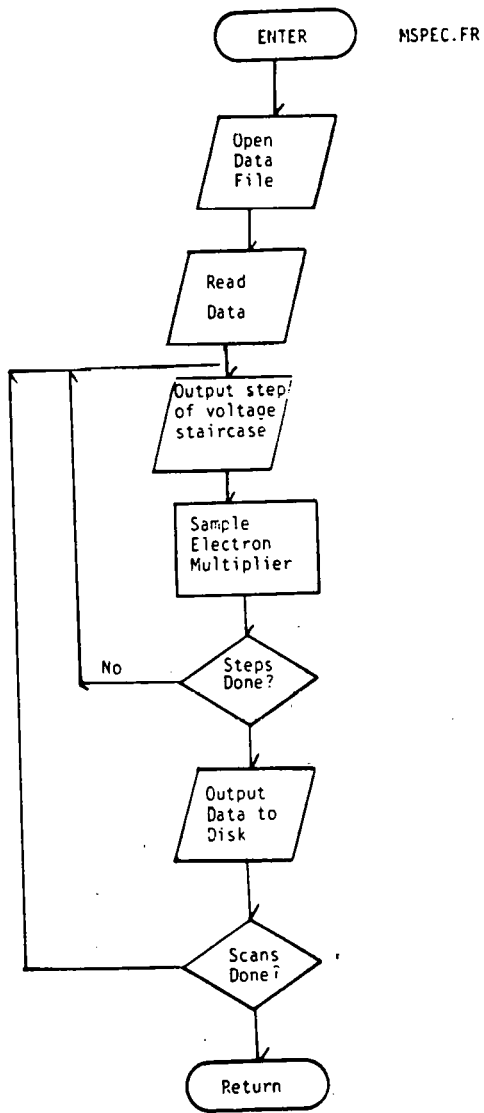


Figure 1-E-22.

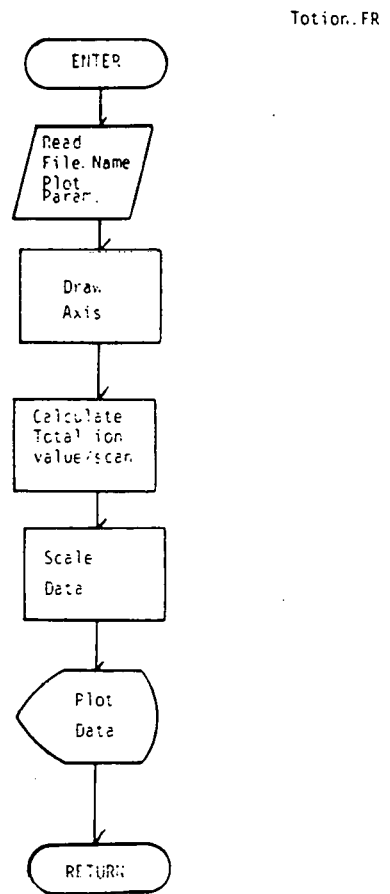


Figure 1-E-23

MSPLT.FR

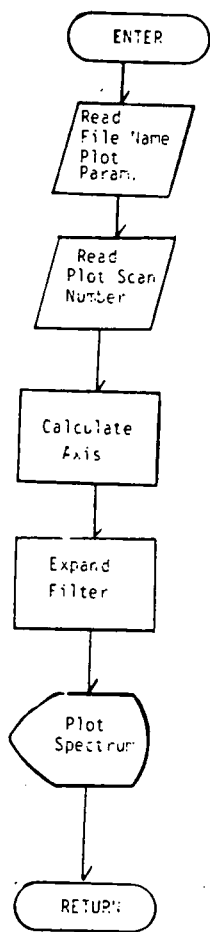


Figure I-E-24

MSSEARCH.FR

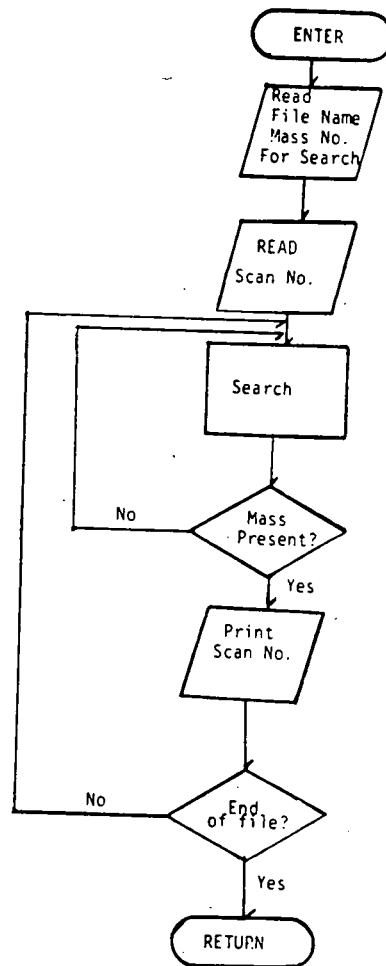


Figure I-E-25

12.6 Section 8 Appendices

12.6.1 Appendix 1 Colony Types of Bacterial
Isolates from the Laboratory
Experiment

12.6.2 Appendix 2 Replica Plating

APPENDIX 1

Colony Types of Bacterial Isolates from the Laboratory Experiment

The criteria for the colony description are given in the following order: size, color, reaction to light, granular or smooth, elevation and border. Size was categorized as small (2 mm or less), medium (2-5 mm), and large (greater than 5 mm). Reaction to light was designated as transparent, translucent, or opaque. The appearance of each colony type was described as rough or smooth and if the colony glistened this was noted. Colony elevation was described as flat, raised, convex, umbonate, or drop-like. The border of the colonies were described as entire (circular with no irregularities), undulating, scalloped, or irregular. The symbols used are numbers 1 through 35 (number of colony isolated), K (growth on Kuwait crude agar), N (growth on naphthalene agar), H (growth on *n*-hexadecane agar), and OZR (growth on OZR medium). Bacteria that metabolized a hydrocarbon or Kuwait crude oil substrate were Gram stained and were reported as Gram positive, Gram negative, or Gram variable, and were classified as either a rod or coccus.

- 1 H: Medium, yellow-green, opaque, smooth, convex, entire, Gram negative rod.
- 2 N: Medium, yellow-orange, opaque, smooth, umbonate, slightly irregular border, Gram positive rod with some filaments present.
- 3 K: Medium, grey-brown, opaque-translucent in rings, smooth, flat, entire, Gram negative rod.
- 4 H: Medium, white, opaque, smooth, raised, entire, Gram positive rod.
- 5 N: Medium-large, white, translucent-opaque, smooth, flat, scalloped-hazy border, Gram negative rod.
- 6 N: Medium, buff, opaque, smooth, convex, entire, no Gram stain, bacterium was lost.
- 7 K: Medium, yellow-green, opaque, smooth, convex, entire, Gram positive rod.
- 8 K: Medium, white, opaque center with translucent border, smooth border with granular center, wrinkled and umbonate, older colonies are starred in center, scalloped border, Gram variable rod.
- 9 N: Medium-large, white, opaque, smooth, raised, starred in center when old, entire, Gram negative rod.
- 10 N: Medium, white, translucent-opaque, smooth and granular center, umbonate, entire, Gram negative rod.
- 11 K: Medium-large, white, translucent to opaque, smooth, slightly umbonate, entire, Gram negative rod.

- 12 N: Medium, yellow, opaque, smooth, glistening, raised, umbonate when old, entire, Gram positive rod.
- 13 HNK: Medium, white, opaque, smooth, umbonate, slightly undulating border, Gram positive coccoid-rod.
- 14 N: Medium, green-yellow, opaque, rough, flat and below the surface of the agar, irregular, Gram positive rod.
- 15 N: Medium, white with brown center, opaque, smooth, flat, scalloped border, Gram variable rod.
- 16 H: Medium, white, opaque, smooth, convex, entire, Gram variable rod.
- 17 H: Medium-large, yellow with buff border, opaque, smooth, and glistening, convex, entire, Gram negative, coccoid to rod shaped.
- 18 N: Medium to large, white, translucent to opaque, smooth, umbonate, undulating, Gram positive rod.
- 19 K.: Medium, white, opaque, smooth, slightly raised, entire, Gram negative coccoid to rod shaped.
- 20 N: Medium, yellow-green, opaque, smooth, convex center with diffuse entire border, Gram positive rod.
- 21 N: Medium, alternating rings of brown, grey, and white, translucent and opaque, smooth, flat, entire, Gram negative rod.
- 22 N: Small to medium, white, opaque, granular, rough, raised, slightly irregular border, Gram positive rod.
- 23 HK: Small to medium, white, translucent to opaque, smooth raised, entire, Gram positive rod.
- 24 NH: Medium, yellow, opaque, smooth, raised, entire, gram positive coccoid to rod shaped.
- 25 K: Small, white-yellow, opaque, smooth, raised, entire, Gram positive rod.
- 26 OZR: Small, white, opaque, smooth, convex, entire.
- 27 OZR: Small, white, opaque, smooth, flat, entire.
- 28 OZR: Small, white, opaque, smooth, flat, entire.
- 29 OZR: Large, green-yellow, translucent to opaque, rough, agarolytic, irregular.
- 30 OZR: Large, brown and white rings, translucent to opaque, smooth, agarolytic, entire.
- 31 OZR: Large, yellow, opaque, smooth, mucoid, convex, entire.

32 OZR: Small, yellow, opaque, smooth, convex, entire.

33 OZR: Medium, white, translucent to opaque, smooth, droplike, entire.

34 OZR: Medium, yellow, opaque, smooth, flat, entire.

APPENDIX 2

Replica Plating: Heterotrophic Bacterial Population diversity and Hydrocarbon Degraders in the Heterotrophic Bacterial Population During the Laboratory Experiment Bacterial colonies on OZR master plates were enumerated by colony type (colony types are given in Appendix 1). Colonies that grew on hydrocarbon replica plates but not on the basal medium control plate are designated by the hydrocarbon plate they grew on. OZR master plates were made from surface, water column, and sediment samples from four aquaria with Narragansett Bay water plus: (1) control, (2) Kuwait crude oil 15 ppm (v/v), (3) Kuwait crude oil 15 ppm (v/v) and 3 ppm (v/v) Corexit 9527, and (4) Corexit 9527 3 ppm (v/v).

Symbols:

- (1) Numbers 1-36: Bacterial isolates as determined by colony morphology (see appendix 1)
- (2) OZR: Master plates with OZR medium
- (3) B: Number of bacteria growing on the basal medium
- (4) N: Naphthalene utilizers
- (5) H: n-Hexadecane utilizers
- (6) K: Kuwait crude utilizers

A. Water Column Samples from oil aquarium.

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate	
0	100	29	24	5		
		32	23	8		
		30	11	7		
		33	3			
		35	3			
		31	17	14		
		28	8			
		27	2			
		34	1			
		14	7			
		11	2			N K
1	66	31	2	2		
		30	11	5		
		32	5	3		
		35	1			
		29	5	4		
		28	32			
		27	5			
		11	4			
		9	1			K N
2	107	30	15	3		
		31	6	2		
		29	15	7		
		32	7	6		
		35	6			
		34	2			
		28	40			
		27	8			
		22	8			K
		7	no data			
10	61	30	1			
		31	5			
		29	10			
		34	9			
		27	3			
		28	33			
14	56	29	51			
		3	1			
		34	2	2		
		28	2			K

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
18	85	31	2		
		19	2		
		29	11	3	
		28	66		
		27	4		
21	84	31	6		
		29	15		
		30	4		
		32	4		
		27	8		
		33	2		
		28	31		
		34	14		

B. Water Column samples from oil and dispersant aquarium.

0	no data				
1	65	31	7	5	
		30	5		
		32	6	5	
		35	4		
		29	18	6	
		27	4		
		28	10		
		12	3		
		19	8		N K
2	121	31	32	24	
		29	44	7	
		32	2	2	
		35	6		
		30	13		
		28	19		
		27	2		
		1	1		H K
11	2				
7	no data				
10	65	31	1		
		29	34		
		32	1		
		38	23		
		19	6		K

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate	
14	89	31	4	2		
		34	1			
		30	2			
		35	1			
		29	78			3
		28	2			
		19	1			K
18	139	31	8			
		35	5			
		34	1			
		29	21			
		27	3			
		28	102			
		22	1			K
21	58	35	8			
		30	1			
		34	4			
		29	12			
		27	6			
		28	22			3
		17	2			H
		19	1			K
		25	2			K

C. Water column samples from dispersant aquarium.

0	52	31	4	3		
		30	13	8		
		32	7			
		29	8	4		
		27	1			
		28	11			
		34	1			
		19	1			K
		21	1			N
		15	3			N
		20	2			N
1	61	31	6	4		
		30	6	3		
		29	23	7		
		32	3	3		
		35	1			
		33	1			
		28	13			
		27	2			

day	total # colonies OZR masters	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
		34	2		
		6	1		N
		11	2		K
		3	1		K
2	37	30	1		
		31	2		
		32	1		
		29	16		
		34	6	1	
		27	2	3	
		28	5		
		24	4		N
7	99	31	8	1	
		30	6		
		35	2	1	
		34	4		
		29	50	6	
		28	18		
		27	5		
		19	5		K
		22	1		K
10	71	31	5		
		32	3		
		29	39	5	
		28	17		
		27	1		
		19	3		K
		22	3		K
14	40	29	28		
		28	6		
		27	3		
		21	1		N
		16	1		H
		19	1		K
18	57	29	4		
		31	2		
		35	2		
		27	8		
		28	40		
		32	1		

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
21	69	31	3		
		29	4	2	
		34	22		
		28	21		
		27	18		
		24	1		

D. Water column samples from control aquarium.

0	66	31	4	2		
		29	13	9		
		32	5	2		
		30	9			
		28	26			
		27	1			
		35	2			
		21	4			
		15	1			
		19	1			
						N N K
1	80	31	6	3		
		30	12	4		
		29	20	5		
		27	8			
		28	21			
		34	3			
		32	7			
		33	1			
		16	1			
		19	1			
						H K
2	36	31	9			
		29	6	1		
		32	4			
		33	1			
		30	1			
		28	9			
		35	3			
		24	1			
		22	2			
						N K
		7	126	31	19	
29	25					
30	4					
35	6					
34	10					
27	7					
28	5					

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
10	79	31	10	2	
		32	3		
		30	5		
		35	1		
		29	14		
		33	1		
		34	3		
		28	37		
		27	5		
14	56	31	2	2	
		32	3		
		30	2		
		29	6		
		27	4		
		28	28		
		34	11		
18	59	31	6		
		35	1		
		29	2		
		28	35		
		27	10		
		34	4		
		17	1		H
21	53	31	5	1	
		29	6		
		30	2		
		32	6		
		27	10		
		28	19		
		34	5		

E. Sediment samples from oil aquarium.

0	65	32	22	6	
		30	4	2	
		35	4		
		33	2		
		29	10	5	
		28	6		
		27	6		
		31	2		
		15	2		N
		16	2		H
		23	1		H
		19	4		K

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate	
1	87	30	3			
		32	24	5		
		29	35	9		
		28	6			
		27	5			
		34	3			
		33	5			
		31	2			
		19	1			K
		3	1			K
		11	2		K	
2	57	30	6	1		
		32	13	5		
		33	4			
		35	4			
		29	16	4		
		27	9			
		28	2			
		34	1			
		19	1			K
		25	1			K
7	70	31	6			
		30	5			
		29	30	10		
		32	5	5		
		35	2			
		28	15			
		27	3			
		4	4			H
10	101	30	5			
		29	30			
		32	15			
		35	4			
		31	2			
		27	24			
		28	21			
14	64	29	32			
		30	3	7		
		32	4			
		35	5			
		27	6			
		28	11			
		33	1	1		
		34	1			
		19	1			K

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
18	46	29	19	7	
		30	1		
		32	5		
		35	3		
		33	7		
		27	5		
		28	6		
		21	61		30
32	4				
33	3				
29	17				
34	7				
28	13				
27	4				
15	2			N	
4	1			H	
19	3			K	
3	2			K	

F. Sediment samples oil and dispersant aquarium.

0	82	30	6	20				
		32	25					
		29	7		4			
		35	21					
		33	7					
		34	4					
		27	3					
		28	5					
		18	1		N			
		19	3		K			
		1	70		30	8	3	
					31	7		
					29	22		7
32	8			8				
35	4							
33	2							
34	2							
27	5							
28	8							
23	1			K, H				
19	2			K				
25	1	K						

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate		
2	83	29	28	12			
		30	6				
		32	11	6			
		33	3				
		35	14				
		28	11				
		27	1				
		34	3				
		19	4				
		7	2			K	
7	126	31	23	23			
7	126	30	1				
		35	3	2			
		32	1	1			
		29	69	15			
		28	16				
		27	2				
		34	2				
		8	9			K	
		10	85	31	12	3	
		10	85	30	3		
29	47			7			
32	8			7			
35	2						
27	5						
28	5						
33	1						
24	1					H,N	
14	105			31	12		
14	105			30	2		
		35	2				
		32	2				
		29	64				
		28	13				
		27	2				
		24	2				
		22	6				
		18	115	31	7	2	
		18	115	32	4		
29	89			13			
28	12						
27	1						
17	1						
22	1					H	
						K	

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
21	62	29	34	3	
		32	1		
		34	3		
		28	7		
		27	17		

G. Sediment samples dispersant aquarium.

0	61	30	7		
		32	14	2	
		35	6		
		34	2		
		29	5		
		27	6		
		28	7		
		12	1		N
		19	7		K
1	60	30	7		
		31	2		
		29	14	6	
		32	15	12	
		35	12		
		33	3		
		34	3		
		28	3		
		27	4		
2	no data				
7	217	31	35	27	
		35	3	3	
		29	124	26	
		34	5		
		27	2		
		28	41		
		10	1		N
		4	4		H
		19	6		K
10	238	31	40	26	
		32	4	1	
		30	1		
		29	146	7	
		27	6		
		28	27		
		34	5		

day	total # colonies OZR master	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
		24	1		N, H N
		15	1		
		23	3		
		22	4		
14	76	31	3	3	
		32	4		
		35	1		
		30	3		
		29	54	4	
		27	2		
		28	9		
18	120	31	1		
		29	110	7	
		28	15		
		27	3		
		16	1		H
21	128	31	7	4	
		32	2	2	
		35	4	4	
		29	87	9	
		27	9		
		28	20		

H. Sediment samples control aquarium.

0	36	33	7		
		32	14	5	
		30	1		
		29	7	1	
		27	3		
		13	1		N, H, K
		19	3		K
1	65	31	7		
		30	7	3	
		32	22	11	
		29	8	3	
		27	11		
		33	4		
		28	5		
		13	1		K

day	total # colonies OZR medium	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate	
2	60	31	15			
		29	11	3		
		32	17	7		
		33	3			
		30	2			
		28	6	3		
		27	4			
		19	2			K
7	217	31	30	2		
		29	104	24		
		34	19	8		
		27	39			
		28	5	3		
		33	1			
		35	8	5		
		5	1			N
		2	2			N
		9	4			N
		14	3			H
19	1			K		
10	231	31	9	2		
		30	7	1		
		29	117	12		
		32	27	3		
		28	33	1		
		27	5			
		33	2			
		34	11			
		35	9			
		14	9			N
		19	2			K
14	121	31	5	1		
		29	65	7		
		32	4	1		
		30	3			
		34	2			
		35	9			
		28	16			
		17	4			H
		27	7			
		22	5			K
18	no data					
21	no data					

I. Surface samples from oil aquarium.

day	total # colonies OZR medium	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
1	95	30	12	8	N N K
		29	15	4	
		27	15		
		28	41		
		32	8	8	
		15	1		
		12	2		
		19	1		
2	153	31	13	13	K
		30	7	7	
		29	18	7	
		27	8		
		28	86		
		32	19	8	
		19	2		
10	110	32	12		
		29	2		
		27	37		
		28	59		
14	35	30	1		
		29	2		
		28	27		
		27	5		
21	73	32	2		
		29	1		
		27	29		
		28	41		

J. Surface samples from oil and dispersant aquarium.

1	50	31	6	2	K
		29	11	2	
		30	5	2	
		32	3		
		27	15	2	
		28	8		
		19	2		

day	total # colonies OZR medium	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate	
2	149	31	55	40		
		29	35	7		
		30	6	3		
		32	3			
		27	9			
		28	37			
		15	2			N
		24	1			N
		13	1			H
10	75	31	9	3		
		30	1	1		
		29	10	2		
		27	28			
		28	10	8		
		18	3			N
		22	14			K
14	44	31	1			
		29	6	2		
		27	14			
		28	23	7		

21 no data

K. Surface samples from dispersant aquarium.

1	92	31	10	10		
		29	25	7		
		27	16	4		
		28	15			
		32	6	3		
		30	5			
		2	3			N
		16	4			H
		19	8			K
2	36	31	2			
		32	2			
		30	1			
		29	3			
		27	24			
		28	4			
10	89	31	12			
		29	11			
		27	33	1		
		28	28	1		
		32	3			
		22	2			K

day	total # colonies OZR medium	colony type	# of each colony type	# colonies growing on basal medium	growth on hydrocarbon substrate
14	30	29	2		
		27	9		
		28	19		
21	93	33	5		
		27+28 (a)	88		

(a) Too difficult to distinguish between colony type 27 and 29 on this plate; therefore combined the totals.

L. Surface samples from control aquarium.

1	98	27	13	4	
		16	11		H
		28	11		
		29	22	8	
		30	6		
		31	14	14	
		32	14	4	
		24	2		N
		7	1		K
		19	4		K
2	56	31	18	2	
		29	8	4	
		27	19	3	
		28	8		
		30	1		
		32	1	1	
		13	1		H
10	87	29	30		
		31	2		
		28	37		
		27	10		
		32	6		
		12	2		N
14	28	29	5	1	
		27	2	1	
		28	20		
		24	1		N
21	71	29	3		
		27	21	1	
		28	46	1	
		31	2		

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KEYW DEEPWATER TERMINALS, DEEP-DRAFT SHIPS,
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- KEYW AEROSOL INSTRUMENT PERFORMANCE, AEROSOL MEASURING INSTRUMENTS, BETA-RAY ABSORPTION
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CODE 70000
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- AUTH ANONYMOUS
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- AUTH ANONYMOUS
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CODE 02300
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- KEYW OIL EATING BACTERIA, NUTRIENTS, CLEANUP
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- AUTH ANONYMOUS
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CODE 20010
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KEYW OIL SPILL CONTAINMENT, REMOVAL
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- AUTH ANONYMOUS
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- AUTH ANONYMOUS
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CODE 05030
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CODE 71110
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TITL THE BRAYD BLOWOUT-IAU REPORT NO. 60
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ABST A COMPENDIUM OF THE INVESTIGATIONS, ANALYSES, AND EVALUATIONS ORGANIZED BY THE CONTINENTAL SHELF INSTITUTION IN CONNECTION WITH THE BRAYD BLOWOUT AT THE END OF APRIL 1977. PART I GIVES A SHORT SUMMARY OF THE RESULTS OF THE INVESTIGATIONS; SOME THOUGHTS OF A CRISIS PLAN. PART 2 IS A DETAILED REPORT OF THE INVESTIGATIONS, ANALYSES AND ASSUMPTION OF WHICH THE IMA AND ITS RESULTS ARE BASED.
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CODE 71120
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CODE 29120
- AUTH ANONYMOUS
TITL CENTER FOR SHORT LIVED PHENOMENA
PUBL 1974 ANNUAL REPORT AND REVIEW OF EVENTS, DEC. 1975
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KEYW EARTHQUAKES, ERUPTIONS, METEORITE FALLS, OIL SPILLS, ANIMAL MIGRATIONS AND IMPESTATIONS

- CCCE 4074E
- AUTH ANONYMOUS
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CODE 7128F
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- AUTH ANONYMOUS
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PUBL USCG, AD 776 957
KEYW CHEMICAL ADDITIVES, CONTROL
CODE 0198F
- AUTH ANONYMOUS
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ABST DISCUSSES THE OBJECTIVES OF A STUDY TO DETERMINE THE OVERALL ENVIRONMENTAL IMPACT FROM OIL SPILLS THROUGH THE PROPER USE OF CHEMICAL AGENTS.
KEYW CHEMICAL AGENTS, DISPERSANTS, ENVIRONMENTAL IMPACT, REDUCTION
CODE 3081F
- AUTH ANONYMOUS
TITL CHEMICAL HAZARDS RESPONSE INFORMATION SYSTEM PROJECT PRELIMINARY SYSTEM PLAN
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CODE 0235F
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TITL CHEMICAL TREATMENT OF OIL SLICKS
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ABST THE EFFECTIVENESS AND POTENTIAL POLLUTIONAL EFFECTS OF CHEMICALS AND OTHER MATERIALS USED TO DISPERSE, SINK, BURN, OR OTHERWISE DISSIPATE OIL SLICKS ARE DISCUSSED.
KEYW CHEMICAL TREATMENT, DISPERSION, SINKING
CODE 0044F
- AUTH ANONYMOUS
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ABST VARIOUS TYPES OF CIRCULATOR BATHS ARE OFFERED.
KEYW CATALOG, CIRCULATOR BATHS, CONTROLLERS
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- AUTH ANONYMOUS
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PUBL INC. JULY 1970
ABST INC. CIVIL LIBERTIES CONVENTION, MEETINGS BEFORE SUB COMMITTEE ON AIR AND WATER POLLUTION, 1968-1969
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- AUTH ANONYMOUS
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PUBL OFFSHORE TECHNOLOGY
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KEYW
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KEYW CLEANUP, OPERATIONS, PROCEDURES
CODE 3024F
- AUTH ANONYMOUS
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TITL COASTAL EFFECTS OF OFFSHORE ENERGY DEVELOPMENT: OIL AND GAS SYSTEMS
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ABST ANALYSIS OF COASTAL EFFECTS AND CONSEQUENCES FOR MAR. AND DEL. OF 3 PROPOSED OFFSHORE ENERGY SYSTEMS.
KEYW OFFSHORE ENERGY SYSTEMS, DEVELOPMENT, CONSTRUCTION
CODE 7070F
- AUTH ANONYMOUS
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PUBL US CONGRESS, OFFICE OF TECHNOLOGY ASSESSMENT, NOV. 1974
ABST AN ASSESSMENT OF OIL AND GAS SYSTEMS, DEEPWATER PORTS AND NUCLEAR POWERPLANTS OFF THE COAST OF NEW JERSEY AND DELAWARE.
KEYW OIL AND GAS SYSTEMS, DEEPWATER PORTS, FLOATING NUCLEAR POWER PLANTS
CODE 7175B, A,B
- AUTH ANONYMOUS
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ABST THE BACKGROUND DETAILS THE SCOPE OF THE CS IN FIGHTING OIL SPILLS AND THE SERVICES AND TESTED EQUIPMENT AVAILABLE FROM CS.
CODE 3054F
- AUTH ANONYMOUS
TITL COLLECTION, UNDERWATER STORAGE, AND DISPOSAL OF PLEASURACRAFT WASTES
PUBL FEDERAL WATER POLLUTION CONTROL ADMINISTRATION, PROGRAM NO. 1502G, SEPT. 1964
ABST THE PROJECT DEMONSTRATED THAT ON-BOARD STORAGE OF WASTE CANNOT BE USED AND SUBSEQUENT DISCHARGE INTO AN UNDERWATER STORAGE TANK WAS EFFECTIVE AND ECONOMICAL. THIS PROJECT SHOWED THAT THE DISCHARGE OF SEWAGE FROM BOATS INTO RIVERS, LAKES, WATERWAYS, AND ESTUARIES COULD BE ELIMINATED.
CODE 3050F
- AUTH ANONYMOUS
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PUBL 93RD CONGRESS, HR 434, FEB. 1973
ABST SECTION BY SECTION ANALYSIS OF PROPOSED ACT CONCERNING COMPENSATION FOR OIL POLLUTION DAMAGE.
CODE 6077F
- AUTH ANONYMOUS
TITL COMPUTER EVALUATES COST OF NORTH SEA BLOWOUT OIL SPILL
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CODE 7053F
- AUTH ANONYMOUS
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CODE 2110F
- AUTH ANONYMOUS
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- AUTH ANONYMOUS
TITL CONCEPT DEVELOPMENT OF A HEAVY DUTY OIL CONTAINMENT SYSTEM FOR USE IN THE HIGH SEAS VOL.1
PUBL ATLANTIC RESEARCH CORP. AD 719 615
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- AUTH ANONYMOUS
TITL CONCEPT DEVELOPMENT OF A HYDRAULIC SKIMMER SYSTEM FOR RECOVERY OF FLOATING OIL
PUBL EPA, PROJECT NO. 15080PH, CONTRACT NO. 14-12-084, APRIL 1971
ABST EXPERIMENTAL WORK HAS DIRECTED TOWARD COMPONENT DEVELOPMENT AND EVALUATION OF A LARGE SYSTEM MODEL

- IN A SIMULATED ENVIRONMENT. OTHER EQUIPMENT SUCH AS AN ULTRASONIC OIL THICKNESS GAUGE, PROLESS PUMPS AND TANKAGE WERE ALSO USED.
- RETR CODE 0052A
- AUTH ANONYMOUS
TITL CONCEPT DEVELOPMENT OF A PROTOTYPE LIGHTWEIGHT OIL CONTAINMENT SYSTEM FOR USE ON HIGH SEAS
PUBL JOHN-MANSVILLE PRODUCTS CORP. AD 722 601
CODE 0172A
- AUTH ANONYMOUS
TITL THE CONDUCT OF A FEASIBILITY STUDY OF THE INVERTED NEIN OIL COLLECTION CONCEPT
PUBL BATTELLE MEMORIAL INSTITUTE
CODE 0189F
- AUTH ANONYMOUS
TITL CONJUNCTION ON SPILL TRAINING
PUBL PETROLEUM ASSOCIATION FOR THE CONSERVATION OF THE CANADIAN ENVIRONMENT (PACE) MAY 1972
ABST LISTS INFORMATION, FILMS AVAILABLE, TRAINING MATERIALS TO IMPROVE RESPONSE CAPABILITIES WITHIN OIL INDUSTRY AND GOVERNMENT. REPRESENTATIVES FROM THE PETROLEUM ASSOCIATION FOR THE CONSERVATION OF THE CANADIAN ENVIRONMENT, THE ONTARIO MINISTRY OF THE ENVIRONMENT, THE CANADIAN COAST GUARD & THE FEDERAL DEPARTMENT OF FISHERIES AND THE ENVIRONMENT REVIEWED SOME OF THE REQUIREMENTS FOR SPILL TRAINING PEOPLE IN CANADA, IN INDUSTRY AND GOVERNMENT.
RETR OIL SPILL, CONTINGENCY GUIDELINES, CLEAN-UP
CODE 7733F
- AUTH ANONYMOUS
TITL CONTINGENCY PLANNING GUIDELINES
PUBL CONSORTIUM ON SPILL TRAINING, PETROLEUM ASSOCIATION FOR THE CONSERVATION OF THE CANADIAN ENVIRONMENT FEBRUARY 1972
ABST THE CONTINGENCY PLANNING GUIDELINES WERE DEVELOPED BY A SUB COMMITTEE OF THE CONSORTIUM ON SPILL TRAINING TO IDENTIFY PERTINENT CONSTITUENTS OF A CONTINGENCY PLAN. THE GUIDELINES WILL ASSIST IN THE PREPARATION OF SPECIFIC CONTINGENCY PLANS FOR SPILLS OF OIL AND OTHER HAZARDOUS MATERIALS.
RETR CONTINGENCY GUIDELINES, OIL SPILL, CLEAN-UP
CODE 7734F
- AUTH ANONYMOUS
TITL CONTINUATION PROPOSAL TO EPA GRANT R 00302016, A FACILITY FOR THE EXPERIMENTAL ANALYSIS OF COASTAL MARINE ECOSYSTEMS
PUBL UMI, CSL
ABST CONTINUATION OF PROGRESS REPORT COVERING PERFORMANCE OF EXPERIMENTAL ECOSYSTEMS SIMULATING A VARIETY OF MARINE ENVIRONMENTS.
RETR ECOSYSTEMS, ECOSYSTEMS, COASTAL MARINE ENVIRONMENT
CODE 7863AF
- AUTH ANONYMOUS
TITL CONTROL AND CONTINUIT OF OIL POLLUTION ON THE BEACH WITH MONITORING AND SAMPLING FILMS
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. 72410.1/4.1, NOV. 1971
CODE 0780H
- AUTH ANONYMOUS
TITL CONTROL OF HAZARDOUS MATERIAL SPILLS
PUBL PROCEEDINGS OF THE 1972 NATIONAL CONFERENCE ON CONTROL OF HAZARDOUS SPILLS, ENVIRONMENTAL SCIENCE, SER. VOL. 1, EPA
ABST PERTAINS TO ALL PHASES OF OIL SPILL CONTROL, PREVENTION, AND CLEANUP.
RETR PREVENTION, CLEANUP, CONTROL
CODE 0054A
- AUTH ANONYMOUS
TITL CONTROL OF HAZARDOUS MATERIAL SPILLS VOL. 1 ENVIRONMENTAL PROTECTION AGENCY
PUBL PROCEEDINGS OF THE 1972 NATIONAL CONFERENCE ON CONTROL OF HAZARDOUS MATERIAL SPILLS
RETR CONTROL SYSTEMS, SPILLS, PREVENTION, RESTORATION
CODE 7769F
- AUTH ANONYMOUS
TITL CONTROL OF OIL AND OTHER HAZARDOUS MATERIALS
PUBL EPA, OFFICE OF WATER PROGRAMS
ABST TOPICS DISCUSSED: TANKERS, OFFSHORE DRILLING, OIL SPILL PREVENTION, CONTROL AND TREATMENT.
RETR TANKERS, OFFSHORE DRILLING, PREVENTION, TREATMENT
CODE 0023P
- AUTH ANONYMOUS
TITL COOPERATIVE HURRICANE REPORTING NETWORK OBSERVATIONS
PUBL US DEPT. OF COMMERCE, WEATHER BUREAU
CODE 2952R
- AUTH ANONYMOUS
TITL A COORDINATED SPILL RESPONSE SYSTEM FOR MAJOR HAZARDOUS
PUBL CLEAN VENTURE
ABST THIS PAPER DESCRIBES THE NATURE OF THE CAPABILITY AVAILABLE FROM CLEAN VENTURE AND ILLUSTRATES A METHOD BY WHICH THAT CAPABILITY CAN BE APPLIED IN A PARTICULAR AREA, NEW YORK HARBOR.
RETR SPILL RESPONSE SYSTEM, CLEAN VENTURE, NEW YORK HARBOR
CODE 0201D
- AUTH ANONYMOUS
TITL CRC PRESS REVIEW
PUBL CRC PRESS INC.
ABST CATALOG - CRC COMPOSITE INDEX FOR CRC HANDBOOKS
RETR CATALOG, INCEE HANDBOOKS
CODE 7473F
- AUTH ANONYMOUS
TITL GAUGE OIL BEHAVIOR ON ARCTIC WINTER ICE
PUBL USCG, AD 754 261, SEPT. 1971
RETR OIL BEHAVIOR, ARCTIC WINTER ICE
CODE 0194R
- AUTH ANONYMOUS
TITL GAUGE OIL TRANSPORTATION SYSTEM VALIDZ, ALASKA TO RIMANG, TA IAS PROPOSEL BY SONIO TRANSPORTATION CO. I
PUBL US DEPT. OF THE INTERIOR, BUREAU OF LAND MANAGEMENT, CHAPTER 4, VOL. 1, 2, 3 CHAPTERS 3-9
ABST THIS IS A DRAFT ENVIRONMENTAL IMPACT STATEMENT.
RETR OIL TRANSPORTATION, ALASKA, ENVIRONMENTAL IMPACT
CODE 7000 ABC
- AUTH ANONYMOUS
TITL GAUGE TANKER POLLUTION ABATEMENT
PUBL EXXON CORP., APRIL 1970
ABST OUTLINES GOALS OF INTERNATIONAL CONVENTION FOR THE PREVENTION OF POLLUTION FROM SHIPS, 1973.
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CODE 2934F
- AUTH ANONYMOUS
TITL CURRENT EPA RESEARCH PROJECTS
PUBL HAZARDOUS MATERIALS SPILLS RESEARCH NEWSLETTER, FEB. 1972
ABST INDEX OF CURRENT EPA PROJECTS.
CODE 3064H
- AUTH ANONYMOUS
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PUBL H.R. REPORT NO. 440, 93RD CONGRESS 1ST SESSION
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- AUTH ANONYMOUS
TITL A DESCRIPTION OF THE ENVIRONMENTAL PROJECTION RESEARCH FACILITY HYDRODYNAMICAL-NUMERICAL MODEL, APPLICATIONS
PUBL EPA LAB., AC 749740
CODE 0411H
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TITL DESIGN AND DEVELOPMENT OF AN OPTIMUM OIL STORAGE CONTAINER FROM THE AIR DELIVERABLE ANTI-POLLUTION TRANSFER SYSTEM - ADAPTS.
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. 714018/7002
CODE 074JR
- AUTH ANONYMOUS
TITL DETERGENTS IN WATER, A BIBLIOGRAPHY
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ABST A COMPILATION OF 262 ABSTRACTS IS PRESENTED DEALING WITH DETERGENTS IN WATER
RETR DETERGENTS, CHEMICAL WASTES, ENVIRONMENTAL EFFECTS
CODE 2521P
- AUTH ANONYMOUS
TITL DETERMINATION OF OIL LOSS RATE FROM HIGH SEAS OIL CONTAINMENT BARRIERS
PUBL USCG, AD 762 334
CODE 0105V
- AUTH ANONYMOUS
TITL THE DETERMINATION OF OIL SLICIA THICKNESS BY MEANS OF MULTIFREQUENCY PASSIVE MICROWAVE TECHNIQUES
PUBL USCG, ADA 001302
RETR THICKNESS, MULTIFREQUENCY PASSIVE MICROWAVES
CODE 0247H
- AUTH ANONYMOUS
TITL DETERMINATION OF THE LEEWAY OF OIL SLICKS
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. CG-0-75
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- AUTH ANONYMOUS
TITL DETERMINE PHYSICAL PARAMETERS WHICH AFFECT OIL SPILL CONTAINMENT
PUBL US EPA SSIE NO. 284-778
CODE 0355R
- AUTH ANONYMOUS
TITL DEVELOPMENT OF A HIGH SEAS OIL RECOVERY SYSTEM, PHASE II PROTOTYPE DESIGN, FABRICATION AND TESTING
PUBL USCG, AD 800353
RETR HIGH SEAS, RECOVERY, DESIGN, FABRICATION, TESTING
CODE 0238R

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 TITLE DEVELOPMENT OF A FLOATING OIL SLICK DETECTOR
 PUBL US RESEARCH, INC. 1973
 CODE 0218K

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 TITLE DEVELOPMENT OF A HIGH SEAS OIL RECOVERY SYSTEM
 PUBL CLEAN SYSTEMS INC. FEB. 1972; AG 759 523 AND AG 759 524
 CODE 01834

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 TITLE DEVELOPMENT OF A HIGH SEAS OIL RECOVERY SYSTEM
 PHASE II APPENDIX II MATERIALS AND COMPONENT TESTS
 PUBL USCG, ADA 00394
 REFS HIGH SEAS, RECOVERY, MATERIALS, COMPONENT TESTS
 CODE 0240R

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 PHASE II APPENDIX III SYSTEM TEST
 PUBL USCG, ADA 00394
 REFS HIGH SEAS, RECOVERY, SYSTEM TEST
 CODE 0241A

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 PHASE III, APPENDIX I, DESIGN STUDIES AND SPECIFICATIONS
 PUBL USCG, ADA 00394
 REFS HIGH SEAS, RECOVERY, DESIGN STUDIES, SPECIFICATIONS
 CODE 0239F

AUTH ANONYMOUS
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 PUBL THE AMERICAN PETROLEUM INSTITUTE COMMITTEE ON ENVIRONMENTAL AFFAIRS, MAY 1973
 ABST A DEVELOPMENT AND REFINEMENT FOR DISPERSANT EFFECTIVENESS
 REFS DISPERSANT EFFECTIVENESS, DEVELOPMENT, REFINEMENT
 CODE 25076

AUTH ANONYMOUS
 TITLE DEVELOPMENT OF A NOVEL HIGH VELOCITY OIL SLICK SKINNER
 PUBL HYDRONAUTICS, INC. JUNE 1974, AG 766 880
 REFS HIGH VELOCITY OIL SLICK SKINNER
 CODE 0190K

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 PUBL AIRCRAFT ELECTROSYSTEMS CO., AZUSA, CAL., NTIS, AD79483, JUNE 1973
 ABST AIRBORNE OIL SURVEILLANCE SYSTEM - CONFIGURE TO ASSIST THE USCG IN ENFORCEMENT OF ANTI-POLLUTION LEGISLATION AND ASSESSMENT/CLEANUP OF ACCIDENTAL SPILLS.
 REFS OIL SURVEILLANCE SYSTEM, CLEANUP
 CODE 3117H

AUTH ANONYMOUS
 TITLE DEVELOPMENT OF A SYSTEM FOR MEASUREMENT OF SURFACE CURRENTS AND OCEAN CURRENT OBSERVATION
 PUBL USCG
 REFS MEASUREMENT, SURFACE CURRENTS, OCEANIC CURRENTS
 CODE 0255H

AUTH ANONYMOUS
 TITLE DEVELOPMENT OF BUOY MOUNTED HYDROCARBON VAPOR SENSORS FOR USE IN LOCAL AREA POLLUTION SURVEILLANCE SYSTEMS
 PUBL US DEPT. OF TRANSPORTATION, USCG, NTIS
 CODE 6518R

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 PUBL USCG, DATED, REPORT NO. TENG/001, 1971, RESPONSE AD 732-676
 CODE 0742B

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 PUBL USCG, AUG. 8, 1971, AG 732-676
 CODE 0150A

AUTH ANONYMOUS
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 CODE 4037H

AUTH ANONYMOUS
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 ABST REPORT ON HUSTON'S BIGGEST OIL SPILL DESPITE ON THE FRENCH SHORELINE
 REFS OIL SPILL, BRITANNY COAST
 CODE 2659F

AUTH ANONYMOUS
 TITLE THE DISASTERS THAT DIDN'T

PUBL BRADON, USA THIRD QUARTER 1977
 ABST A REPORT ON OIL SPILLS.
 CODE 7518R

AUTH ANONYMOUS
 TITLE DISPERSANTS INFORMATION FILE
 PUBL VARIOUS
 ABST LETTERS AND PAMPHLETS REGARDING INFORMATION ON DISPERSANTS
 REFS DISPERSANTS, LETTERS, GENERAL INFORMATION
 CODE 5084F

AUTH ANONYMOUS
 TITLE DISPOSAL IN THE MARINE ENVIRONMENT (AN OCEANOGRAPHIC ASSESSMENT)
 PUBL NATIONAL ACADEMY OF SCIENCES
 ABST THIS STUDY REVIEWS AND INTEGRATES SCIENTIFIC AND TECHNICAL INFORMATION ON OCEAN DISPOSAL TO DEVELOP CONCEPTS FOR MONITORING AND REGULATING THIS PRACTICE. THE OBJECTIVE IS TO PROVIDE AS A BASIS FOR EPA'S FUTURE REGULATORY DECISIONS A RATIONALE THAT CONSIDERS OCEAN DISPOSAL IN TERMS BOTH OF THE NEED FOR OCEAN DISPOSAL AND OF THE CAPACITY OF THE MARINE ECOSYSTEM TO RECEIVE WASTES. IT DESCRIBES CURRENT LEGISLATION AND REGULATIONS, THE AMOUNT AND PROPERTIES OF WASTE MATERIAL AND THE PROCESSES THAT AFFECT THEIR FATE AND DISTRIBUTION IN THE MARINE ENVIRONMENT.
 REFS OCEAN DISPOSAL, LEGISLATION, OCEAN POLLUTION
 CODE 7718 F

AUTH ANONYMOUS
 TITLE DISTRIBUTION OF VOLATILE HYDROCARBONS
 PUBL UNKNOWN
 ABST CHARTS OF VOLATILE HYDROCARBONS, INCLUDING AROMATICS, IN PACIFIC OCEAN WATER.
 REFS VOLATILE HYDROCARBONS, CHARTS, AROMATICS
 CODE 2967F

AUTH ANONYMOUS
 TITLE DOCTORAL DISSERTATIONS ON CIVIL ENGINEERING
 PUBL UNIVERSITY MICROFILMS INTERNATIONAL
 ABST 1970-1974 DISSERTATIONS - A BIBLIOGRAPHY
 REFS DISSERTATIONS, BIBLIOGRAPHY
 CODE 7671F

AUTH ANONYMOUS
 TITLE ECU-1 DISPERSING AGENT
 PUBL DUTCH PRIDE PRODUCTS
 ABST USE OF ECU-1 AS A DISPERSANT IS SHOWN. LICENSE CERTIFICATES FOR OIL SPILL CLEAN AGENT FROM STATE OF CAL., ILL. MASS. ARE PRESENTED.
 REFS DISPERSING AGENT, LICENSES, ECU-1
 CODE 7650F

AUTH ANONYMOUS
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 PUBL USEPA, 220/1-79-001A, 69-01-1341 NC, 20, JULY 1975
 ABST THE PURPOSE OF THE STUDY WAS TO ANALYZE THE ECONOMIC IMPACT OF THE F-0-P-G-A
 REFS INTERNATIONAL REGULATIONS, WASTE TREATMENT CONTROLS, COSTS
 CODE 6570F

AUTH ANONYMOUS
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 REFS WAVES, OIL SPILL MOVEMENTS, EFFECTS
 CODE 0192R

AUTH ANONYMOUS
 TITLE THE EFFECTS OF CURRENTS AND WAVES ON AN OIL SLICK RETAINED BY A BARRIER
 PUBL USCG, ADA 004075
 REFS CURRENTS, WAVES, BARRIER
 CODE 02433

AUTH ANONYMOUS
 TITLE EFFECTS OF CURRENTS AND WAVES ON FLOATING OIL SLICKS RETAINED BY A BARRIER
 PUBL TEXAS A&M UNIV. FOR USCG, SSIE NO. 62-63
 CODE 0440B

AUTH ANONYMOUS
 TITLE EFFECTS OF OIL AND CHEMICALLY DISPERSED OIL ON SELECTED MARINE BIOTA - A LABORATORY STUDY
 PUBL APL, REPORT NO. 4141, NOV. 1973
 ABST THIS REPORT CONCLUDES A TWO YEAR DEVELOPMENT STUDY ON ACUTE, CHRONIC AND SUBLETHAL EFFECTS OF OIL UPON MARINE BIOTA USING A REFINED OIL AND TWO CRUDE OILS. EFFECTS WERE BIODIAGNOSED WITH UNDISPERSED AND DISPERSED OILS.
 REFS DISPERSANTS, TOXICITY, MARINE BIOTA
 CODE 2891F

AUTH ANONYMOUS
 TITLE ENERGY AND ENVIRONMENTAL GOALS: COMPATIBILITY THROUGH ENVIRONMENTAL CONTROLS
 PUBL U. S. OIL ENVIRONMENTAL CONTROL SYMPOSIUM
 ABST DOCUMENT CONSISTS OF ABSTRACTS FROM THE ABOVE NAMED SYMPOSIUM.
 REFS OIL SPILL, ENVIRONMENT, RECOVERY
 CODE 7714 F

AUTH ANONYMOUS
 TITL ENERGY SYSTEMS OF EXTENDED DURANCE IN THE 1-100
 KILOWATT RANGE FOR UNDERSEA APPLICATIONS
 PUBL NAVAL UNDERWATER SYSTEMS CENTER, NATIONAL ACADEMY
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 ABST THIS REPORT PRESENTS A DISCUSSION OF REQUIREMENTS
 AS WELL AS THE PRESENT AND PROSPECTIVE TECHNOLOGY
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 APPLICATIONS.
 REVD FUEL SUPPLY SYSTEMS, ENERGY CONSERVATION, HEAT
 TRANSFER
 CODE 05231

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 PUBL OCEAN SYSTEMS DIVISION, LOCKHEED MISSILES AND
 SPACE CO., AD 725 003
 CODE 0188R

AUTH ANONYMOUS
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 FOR OPEN OCEAN SPILLS
 PUBL WILLIAM P. BISHOP ASSOCIATES AD 723 000
 CODE 0190R

AUTH ANONYMOUS
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 VERSUS UNTREATED SPILLS
 PUBL WRI, WASH. APR. 30, 1979
 ABST A PROPOSAL FOR RESEARCH ON ENVIRONMENTAL
 ASSESSMENT OF TREATED OIL SPILLS VERSUS UNTREATED
 SPILLS.
 REVD PLANNING AND ANALYSIS, EXPERIMENTAL ASSESSMENT,
 ENVIRONMENTAL ASSESSMENT, TREATED, UNTREATED
 CODE 0084B

AUTH ANONYMOUS
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 RESEARCH AND DEVELOPMENT ADMINISTRATION CONTRACTOR
 SITES, CALENDAR YEAR 1975, VOL. 3 OF 3
 PUBL DIVISION OF SAFETY, STANDARDS AND COMPLIANCE,
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 70-1041975104-11
 ABST THE PURPOSE OF THIS COMPILATION IS TO PRESENT IN A
 CENTRAL REFERENCE DOCUMENT ALL OF THE INDIVIDUAL
 ANNUAL REPORTS SUMMARIZING THE RESULTS OF THE
 ENVIRONMENTAL MONITORING PROGRAMS CONDUCTED AT
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 ENVIRONMENTAL IMPACT OR WHICH RELEASE A
 SIGNIFICANT QUANTITY OF RADIOACTIVITY OR
 NONRADIOACTIVE POLLUTANTS.
 REVD ANNUAL REPORTS, ENVIRONMENTAL MONITORING
 CODE 0178D

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 TITL ENVIRONMENTAL RESEARCH ANNUAL REPORT
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 ABST THIS REPORT SUMMARIZES COMPLETED API RESEARCH AND
 COMPLETED APRIL RESEARCH, AS WELL AS ON-GOING API
 PROJECTS.
 REVD REMOVAL, SKIMMERS, TOXICITY, SOLVENT RECOVERY
 CODE 2400F

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 ABST THIS REPORT IS THE SECOND OF A SERIES OF ANNUAL
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 REVD RESEARCH MANAGEMENT, OIL POLLUTION, WATER
 POLLUTION, SOLID WASTE
 CODE 0595F

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 ABST GEOPHYSICAL INVESTIGATIONS ON LONGITUDINAL
 CIRCULATION AND MIXING RELATIONS IN ESTUARIES
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 CIRCULATION TURBULENT PROCESSES IN ESTUARIES THE
 COASTAL BOUNDARY LAYER, THE LAST SIX PAPERS
 ENGINEERING AND ENVIRONMENTAL ASPECTS EXTEND THE
 DISCUSSION INTO THE AREAS OF THE CHEMISTRY AND
 BIOLOGY OF THE ESTUARINE CIRCULATION AND OF THE
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 REVD CIRCULATION, TURBULENCE, BIOGEOCHEMICAL MODELS
 CODE 7717 F

AUTH ANONYMOUS
 TITL EVALUATION OF AN INFRARED OIL FILM MONITOR
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 REVD EVALUATION, INFRARED OIL FILM MONITOR
 CODE 0250R

AUTH ANONYMOUS
 TITL EVALUATION OF AN INFRARED OIL FILM MONITOR
 PUBL WRIGHT AND WRIGHT ENV. ENG., NOV. 1973, AD 770 814
 CODE 0222R

AUTH ANONYMOUS
 TITL EVALUATION OF AN INFRARED OIL FILM MONITOR

PUBL WRIGHT AND WRIGHT ENVIRONMENTAL ENGINEERING FOR
 USCG, SSIE NO. G2-80339
 CODE 0063R

AUTH ANONYMOUS
 TITL EVALUATION OF CONCEPTS FOR SEPARATING OIL FROM
 WATER DISCHARGED FROM SHIPS
 PUBL USCG, G-DIT-1, AUG. 1973, AD 770 200
 CODE 0233R

AUTH ANONYMOUS
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 THE RESTORATION OF OIL-CONTAMINATED BEACHES
 PUBL DEPT. OF THE INTERIOR, OCT. 1970
 REVD EARTH MOVING EQUIPMENT, RESTORATION, BEACHES
 CODE 0040R

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 OF POLLUTION CONTROL BARRIERS
 PUBL ADA 004074
 REVD STRENGTH, SEAKEEPING ABILITIES, CONTROL BARRIERS
 CODE 0237R

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 ABST A LISTING OF ESTUARIAL PROJECTS TO BE FUNDED IN
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 POLLUTION, INDUSTRIAL POLLUTION
 CODE 0020R

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 COASTAL MARINE ECOSYSTEMS
 PUBL EPA PROPOSAL 0017650, SUBMITTED 3/31/75
 ABST THE PRIMARY OBJECTIVE OF THE PROPOSAL IS TO
 DESIGN, DEVELOP AND OPERATE A FACILITY FOR THE
 EXPERIMENTAL ANALYSIS OF COASTAL MARINE
 ECOSYSTEMS.
 REVD COASTAL MARINE ECOSYSTEMS, RESEARCH, ENVIRONMENTAL
 STRESSSES
 CODE 7070F

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 COASTAL MARINE ECOSYSTEMS, YEARS 2 AND 3.
 PUBL TECHNICAL PROGRESS REPORT AND CONTINUATION
 PROPOSAL, EPA GRANT, NO. 000306/020, MARINE
 ECOSYSTEMS RESEARCH LAB., WRI GRAD. SCHOOL OF
 OCEANOGRAPHY, 1970-1977
 ABST THIS IS A STUDY ON EXPERIMENTAL MARINE ECOSYSTEMS.
 REVD ECOSYSTEMS, BEHAVIOR, SPECIES, ELEMENTS
 CODE 00590

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 CONTROL EQUIPMENT A FEASIBILITY STUDY
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
 NO. 12412.1/2, JAN. 1973
 REVD FAST DELIVERY SYSTEM, CONTROL
 CODE 0780F

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 TITL THE FATE OF OIL SPILLS AT SEA
 PUBL GOVERNMENT REPORT ANNOUNCEMENTS
 CODE 0326R

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 ABST ACQUISITION AND INTERPRETATION OF MULTISPECTRAL
 AERIAL PHOTOGRAPHY AND THERMAL INFRARED IMAGERY
 WAS PERFORMED TO EVALUATE REMOTE SENSING
 APPLICATIONS TO OIL AND OTHER HAZARDOUS SPILL
 PREVENTION SURVEILLANCE.
 REVD SURVEILLANCE, MULTISPECTRAL AERIAL PHOTOGRAPHY,
 THERMAL INFRARED IMAGERY
 CODE 0030R

AUTH ANONYMOUS
 TITL THE FEASIBILITY OF SURFACE SKIMMING OIL COLLECTION
 DEVICES
 PUBL THE CHARLES RIVER ASSOCIATION, AD 710 324
 CODE 0102R

AUTH ANONYMOUS
 TITL A FEASIBILITY STUDY OF THE USE OF THE OLEOPHILIC
 BELT OIL SCRUBBER
 PUBL SMALL PIPELINE CORP. AD 723500
 CODE 0100R

AUTH ANONYMOUS
 TITL A FEASIBILITY ANALYSIS OF INCINERATION SYSTEMS FOR
 RESTORATION OF OIL CONTAMINATED BEACHES
 PUBL EPA, PROGRAM NO. 150802E, CONTRACT NO. 14-12-505
 ABST THE FEASIBILITY OF EMPLOYING A COMBUSTION PROCESS
 FOR RESTORING OIL CONTAMINATED BEACHES WAS
 INVESTIGATED.
 REVD INCINERATION SYSTEMS, RESTORATION, CONTAMINATED
 BEACHES
 CODE 0051R

- AUTH ANONYMOUS
 TITLE FEDERAL AND LOCAL RESPONSE TO AN OIL SPILL IN RE-
 SPECT TO GOVERNMENT RESEARCH AND DEVELOPMENT
 PROGRAMS, A LIST OF MAJOR OIL SPILLS, VARIOUS
 CHARTS, OIL SPILL STATISTICS
 PUBL UNANON
 ABST THIS PAPER DISCUSSES FEDERAL AND LOCAL RESPONSE TO
 AN OIL SPILL.
 KEYW FEDERAL RESPONSE, LOCAL RESPONSE, GOVERNMENT
 RESEARCH, CHARTS
 CODE 7040F
- AUTH ANONYMOUS
 TITLE FERTILIZER THAT REDUCES OIL SLICKS DEVELOPED BY
 THE NAVY
 PUBL UNANON
 ABST A SPECIAL FERTILIZER FORMULA, FOR USE ON FLOATING
 OIL SLICKS THAT IMPROVES BY TEN-FOLD THE NATURAL
 BIODEGRADATION PROCESS, HAS BEEN DEVELOPED BY A
 NAVY RESEARCH PROGRAM.
 KEYW BACTERIAL DEGRADATION, GROWTH STIMULATION, CLEANUP
 CODE 7007F
- AUTH ANONYMOUS
 TITLE FIGHTING POLLUTION: LATEST GOVERNMENT ACTION IS
 AIMED AT REDUCING OIL SPILLS AND DISCHARGE
 MARINE ENGINEERING LAB., 1974
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 CODE 0392H
- AUTH ANONYMOUS
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 MARTIN MARITTEA CORP., DEC. 1973, AD A 003031
 CODE 0180A
- AUTH ANONYMOUS
 TITLE FINAL ENVIRONMENTAL IMPACT STATEMENT: REGULATIONS
 FOR U.S. TANK VESSELS CARRYING OIL IN FOREIGN
 TRADE AND FOREIGN TANK VESSELS THAT ENTER THE
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 PUBL USCG, DEPT. OF TRANSPORTATION, OFFICE OF MARINE
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 ABST THIS STATEMENT ASSESSES THE ENVIRONMENTAL IMPACT
 OF CHANGING THE POLLUTION PREVENTION REQUIREMENTS.
 KEYW PREVENTION, OIL TANK VESSELS, MARINE ENVIRONMENTAL
 PROTECTION
 CODE 1012F
- AUTH ANONYMOUS
 TITLE FINAL ISSUE - ORO PUBLICATIONS SUMMARY
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 KEYW BIBLIOGRAPHY, FINAL REPORTS, GRANT, CONTRACT,
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- AUTH ANONYMOUS
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 ABST REPORT OF STUDIES AND INVESTIGATION OF CAUSE AND
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 SOUTH TERNARIE BAY
 CODE 0000A
- AUTH ANONYMOUS
 TITLE FINAL REPORT, MARKING THE SEA SURFACE WITH
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 SEARCH AND RESCUE OF OCEAN DUMPING SURVEILLANCE
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 KEYW SURFACE FILMS, SEA MARKERS, SEARCH AND RESCUE
 CODE 0521F
- AUTH ANONYMOUS
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 PUBL U.S. DEPT. OF THE INTERIOR, GEOLOGICAL SURVEY, PES
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 KEYW EXPLORATION, CONTINENTAL SHELF
 CODE 2520B
- AUTH ANONYMOUS
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 ABST THIS STATEMENT ASSESSES THE ENVIRONMENTAL IMPACT
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 IN TITLE 33, CODE OF FEDERAL REGULATIONS.
 KEYW OIL TANK VESSELS, SEGREGATED BALLAST, PROTECTION,
 REGULATIONS
- CODE 0593F
- AUTH ANONYMOUS
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 OF OIL AND WATER, INSTALLED IN THE NETHERLANDS
 PUBL HOLLAND SHIPBUILDING
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- AUTH ANONYMOUS
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 PUBL EPA, CONTRACT NO. 14-12-900, AUG. 1970
 KEYW FLEXIBLE HOLDING TANK, PLEASURE CRAFT, SANITARY
 SYSTEM
 CODE 0008A
- AUTH ANONYMOUS
 TITLE FLOATING OIL RECOVERY DEVICE
 PUBL EPA PROJECT NO 15000PAC, CONTRACT NO. 14-12-903
 ABST PLOW BENCH TESTS OF A MODEL ROTATING BELT-COULTE
 PLOW OIL RECOVERY DEVICE WERE CONDUCTED IN A CALM
 WATER ENVIRONMENT PRIMARILY ALTHOUGH SOME TESTS
 WERE MADE IN WAVES. ANALYSIS WAS CONDUCTED TO
 DESIGN A CATAMARAN VESSEL SUITABLE FOR MOUNTING
 THE OIL PICKUP UNIT.
 KEYW RECOVERY DEVICES, CATAMARANS, CALM WATERS AND
 WAVES
 CODE 0050F
- AUTH ANONYMOUS
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 PUBL SURFACE SEPARATION SYSTEMS, INC. BULLETIN 10-A
 ABST THIS ADVERTISEMENT DESCRIBES MODEL BU-213M
 OIL SKIRMER. INCLUDES VARIOUS SPECIFICATION AND
 PHOTOGRAPHS.
 CODE 3007F
- AUTH ANONYMOUS
 TITLE FLOATING OIL SKIRMER
 PUBL SURFACE SEPARATION SYSTEMS, INC. BULLETIN NO. 26C
 ABST THIS ADVERTISEMENT DISCUSSES MODEL BU-213M AND
 CONTAINS THE SPECIFICATION OF THE MODEL AS WELL AS
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 RECOVERERS.
 CODE 3000A
- AUTH ANONYMOUS
 TITLE FLOATING OIL SPILL BOOMS: THEIR USE FOR
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 PUBL REPRINTED FROM THE OILER AND HARBOR AUTHORITY, VOL.
 111, NO. 498, APRIL 1962
 ABST THIS ARTICLE DISCUSSES THE USE OF FLOATING OIL
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 PERMANENT BARRIERS PROVIDING CATCHMENT AREAS IN
 THE PREVENTION OF SPILLS AND MOST LIKELY TO COLLAPSE.
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 CANAL AS A SATISFACTORY TYPE BOOM.
 CODE 3000A
- AUTH ANONYMOUS
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 CODE 0300A
- AUTH ANONYMOUS
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 KEYW GELLING, SOLIDIFICATION, CRUDE OILS, TANKERS
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- AUTH ANONYMOUS
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 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
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 TITLE THE GEODE'S BANK PET. STUDY - IMPACT ON NEW
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 PUBL MIT SEA GRANT PROG. MIT, REPORT NO. MITSG 73-5,
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- AUTH ANONYMOUS
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 ABST CATALOG ORDER FORMS
 CODE 2502F
- AUTH ANONYMOUS
 TITLE GUIDE TO WATER CLEANUP, MATERIALS AND METHODS

PUBL ARTHUR G. LITTLE, INC.
 ABST THE OBJECTIVE OF THE GUIDE HAS BEEN TO INCLUDE THE IMPORTANT DOMESTIC AND FOREIGN PRODUCERS OF WATER CLEANUP EQUIPMENT AND MATERIALS + AND TO DESCRIBE THEIR FUNCTION, PROPERTIES, DIMENSIONS, PERFORMANCE CHARACTERISTICS AND APPLICATIONS.
 REYN CLEANUP EQUIPMENT PRODUCERS, FUNCTIONS, PROPERTIES, PERFORMANCE
 CCDE 82000

AUTH ANONYMOUS
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 PUBL US DEPT. OF THE NAVY
 ABST THIS BODALLET CONTAINS A REPAIR MANUAL, TABLE OF CONTENTS, FIFTY FOOT BOOM SECTION DESIGN DRAWING, GUIDANCE FOR BOOM DEPLOYMENT AND CARE, AND AN OIL BOOM ANALYSIS SHEET.
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 CCDE 7831F

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 ABST WORKSHOP TO EXAMINE THE MUTUAL MARITIME PROBLEMS ARISING FROM THE CONDUCT OF SHIPPING AND RELATED ACTIVITIES IN AREAS OF ACTUAL OR POTENTIAL CONGESTION.
 REYN MARITIME COMMERCE, MARITIME RISK, SHIPPING
 CCDE 80100

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 TITL HEAVYWEIGHT OIL CONTAINMENT SYSTEM
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 REYN HEAVYWEIGHT OIL, CONTAINMENT
 CCDE 8242F

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 CCDE 2002F

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 CCDE 7074F

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 ABST THIS IS A UNIQUE COMPILATION OF CURRENT ENERGY RELATED RESEARCH AND DEVELOPMENT.
 REVD INVENTORY, RESEARCH, DEVELOPMENT
 CODE 4017B
- AUTH ANONYMOUS
 TITLE INVESTIGATION OF OIL FLOUORESCENCE AS A TECHNIQUE FOR REMOTE SENSING OF SPILLS
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 CODE 0205A
- AUTH ANONYMOUS
 TITLE INVESTIGATION OF THE USE OF A WATER FLOW TO SEPARATE OIL FROM AN OIL WATER MIXTURE
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- AUTH ANONYMOUS
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 ABST THIS MEETING COVERED THE ITEMS OF THE OFFICIAL AGENDA.
 KEYS LEASING, SALES
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 ABST THIS ADVERTISEMENT RECOMMENDS A TYPE OF TUBING APPLICABLE TO AERATION, OXYGENATION, DIFFUSION OF LIQUIDS AND GASES, AND FILTRATION AND DIALYSIS PROCESSES.
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 CODE 04728

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 ABST DISCUSSES THE PURPOSE AND PHILOSOPHY OF THE ASTM AND PROPOSES STANDARDS ON OIL CLEANUP SYSTEMS. THE ARTICLE ALSO INCLUDES A LISTING OF THE MEMBERS, THEIR ADDRESSES AND THE ORGANIZATIONS THEY REPRESENT.
 CODE 30708

AUTH ANONYMOUS
 TITLE MISCELLANEOUS STATISTICS
 PUBL REPRODUCES COPIES OF LOCATION OF OIL SPILLS, SUMMARY OF TERMINAL SURVEY, VARIOUS CALCULATIONS AS TO SPILL SIZE.
 CODE 30728

AUTH ANONYMOUS
 TITLE MICROWAVE RADIOMETRIC DETECTION OF OIL SLICKS
 PUBL AIRDEF GENERAL CORP., BU 7-2 402
 CODE 02108

AUTH ANONYMOUS
 TITLE MOMENTUM AND MASS TRANSFER IN STRATIFIED FLOWS
 PUBL DEPT. OF MECHANICAL ENG., ILL. 1974
 ABST AS PART OF A STUDY ON THE EFFECTS OF STRAT. DENSITY GRADIENTS ON STEADY AND NON-STEADY FLOWS A LITERATURE SURVEY WAS PERFORMED. THIS STUDY IS INCORPORATED IN A BASIC RESEARCH PROGRAM.
 KEYS EXPERIMENTAL DATA, TURBULENCE THEORIES, INTERNAL WAVES
 CODE 25737

AUTH ANONYMOUS
 TITLE MULTI-SENSOR DETECTION AND TRACKING OF CONTROLLED OIL SPILLS
 PUBL SPECTRUM, INC. JUNE 1971, AD 741 953
 CODE 02068

AUTH ANONYMOUS
 TITLE NATIONAL CONTINGENCY PLAN - REGION I, OIL AND HAZARDOUS SUBSTANCES POLLUTION CONTINGENCY PLAN FOR INLAND NAVIGABLE WATERS, VOLUMES 1-7
 PUBL USEPA, DIVISION OF SURVEILLANCE AND ANALYSIS, JAN. 1972
 ABST THIS PLAN PROVIDES FOR A PATTERN OF LOOK-OUT/INITIAL AND INTEGRATED-RESPONSES TO POLLUTION SPILLS BY DEPARTMENTS AND AGENCIES OF THE FEDERAL GOV'T.
 KEYS ASSIGNMENTS OF DUTIES, ESTABLISH STRIAL POLICES, SYSTEM OF SURVEILLANCE
 CODE 4026,4,8

AUTH ANONYMOUS
 TITLE NATIONAL ENVIRONMENTAL RESEARCH CENTER ANNUAL REPORT, 1974
 PUBL USEPA, 470/4-75-002, MARCH 1975
 ABST ANNUAL REPORT - VARIOUS ARTICLES
 KEYS ANNUAL REPORT
 CODE 60017

AUTH ANONYMOUS
 TITLE NAVAL RESEARCH REVIEWS, JAN. 1976
 PUBL DEPT. OF THE NAVY
 ABST THIS BULLETIN CONTAINS VARIOUS ARTICLES, IN PARTICULAR "NEW SYSTEM ABSORBS OIL SPILLS", RESEARCH NOTES.
 KEYS RECOVERY, BIODIFFUSION-BARRIER, HARVESTER
 CODE 05127

AUTH ANONYMOUS
 TITLE NAVY PROPOSES NEW WEAPONS TO COMBAT HARBOR OIL SPILLS
 PUBL NAVY ENGINEER CIVIL NEWS, VOL. 81, NO. 8, AUG. 1970
 ABST THE NAVY TESTS THREE NEW WAYS FOR CLEANING UP HARBOR OIL SPILLS SUCTION TYPES AND BACTERIALS.
 CODE 30688

AUTH ANONYMOUS
 TITLE NEW IDEA: PROCESS LAUDE OIL WHILE TANKER IS AT SEA
 PUBL OCEAN INDUSTRY, VOL. 5, NO. 7, JULY 1970
 ABST DUE TO JAPAN'S PROBLEM WITH AVAILABLE LAND AREA, THE JAPANESE HAVE COME UP WITH A PLAN TO REFIN. OIL ONBOARD THE TANKERS IN TRANSIT. IT DISCUSSES THE OUTLINE OF THE PLAN, INCLUDING COST, ADVANTAGES, ETC.
 KEYS AVAILABLE LAND AREA, TANKERS, REFIN. OIL
 CODE 30278

AUTH ANONYMOUS
 TITLE NEW OIL SPILL BOOM ANNOUNCED
 PUBL OIL AND GAS JOURNAL, 1974
 CODE 03638

AUTH ANONYMOUS
 TITLE NEW SIMULATED OIL-SPILL TEST TANK
 PUBL OIL AND GAS JOURNAL 1975
 CODE 03668

AUTH ANONYMOUS
 TITLE THE NEW YORK BIGHT PROJECT 1975 STONY BROOK LONG ISLAND, NEW YORK
 PUBL MARINE ECOSYSTEMS ANALYSIS PROGRAM, US DEPT. OF

COMMERCE, PB265280, MARCH 1976
 ABST THIS IS A REPORT ON THE NEW YORK BIGHT PROJECT TO
 MEASURE THE IMPACT OF RAIN IN THE MARINE
 ENVIRONMENT.
 (KEY) BASELINE STUDIES, RESOURCES DEVELOPMENT, WATER
 QUALITY CONTROL
 CODE 05922

AUTH ANONYMOUS
 TITL NO TITL
 PUBL ACME PRODUCTS CO., MARCH 22, 1973
 ABST BULLETINS, SPECIFICATIONS AND PRICES ON THE TOTAL
 PACKAGE AS MOST WIDELY USED FOR CLEANUP OPERATIONS
 FOR OIL SPILLAGES.
 CODE 00178

AUTH ANONYMOUS
 TITL NO TITL
 PUBL OIL AND HAZARDOUS MATERIALS RESEARCH NEWSLETTER,
 MAY 1970
 ABST DEALS WITH OIL SPILLS CONTAINMENT AND CLEANUP AND
 LEGISLATION ALL TOPICS DISCUSSED BRIEFLY.
 CODE 30018

AUTH ANONYMOUS
 TITL NO TITL
 PUBL RI INTERAGENCY POLLUTION ABATEMENT COMMITTEE
 A SURVEY ON COMMUNITIES, THEIR COMMUNICATION
 FACILITIES AND AUTHORIZATIONS TO USE EQUIPMENT.
 CODE 30119

AUTH ANONYMOUS
 TITL NO TITL
 PUBL SLICKWAP INC., SAUGHTUCKER STATION, WESTPO-1, COAR.
 ABST CALCULATION OF WIND DRIVEN CURRENTS, FORCE OF
 WAVES, PERPENDICULAR TO CURRENT FLOW AND TOTAL
 LOADS.
 CODE 00038

AUTH ANONYMOUS
 TITL NOTES ON INDUSTRY'S OIL SPILL CONTROL ACTIVITIES
 POLLUTION CONTROL REPORT
 PUBL OCEAN INDUSTRY, JUNE 1970
 ABST THIS ARTICLE DEALS WITH THE OIL INDUSTRY APPROACH
 TO OIL SPILL POLLUTION, THEIR DEVICES AND THE
 LEGAL PROCESSES NEEDED TO AID IN OIL SPILL
 PREVENTION.
 (KEY) INDUSTRY, DEVICES, LEGAL PROCESSES
 CODE 30258

AUTH ANONYMOUS
 TITL RESEARCH ECOLOGY OF THE MARINE ENVIRONMENT VOL.
 2 DEC. 1974-MARCH 1976
 PUBL NTIS U.S. DEPARTMENT OF COMMERCE
 ABST THE SELECTED ABSTRACTS OF GOVERNMENT-SPONSORED
 RESEARCH REPORTS COVER SALT WATER ECOLOGY OF
 SHELLFISH, FISHES, AQUATIC PLANTS, AQUATIC
 ANIMALS, AND AQUATIC MICROORGANISMS. ESTUARY
 STUDIES ARE INCLUDED. POLLUTION EFFECTS ARE
 INCLUDED EXCEPT FOR REPORTS DEALING WITH
 PESTICIDES AND OIL POLLUTION.
 (KEY) ESTUARY STUDIES, POLLUTION EFFECTS
 CODE 77817

AUTH ANONYMOUS
 TITL RESEARCH ECOLOGY OF THE MARINE ENVIRONMENT VOL.
 3 APRIL 1976-MAY 1977
 PUBL NTIS U.S. DEPARTMENT OF COMMERCE
 ABST THE SELECTED ABSTRACTS OF RESEARCH REPORTS COVER
 SALT WATER ECOLOGY OF SHELLFISH, FISHES, AQUATIC
 PLANTS, AQUATIC ANIMALS, AND AQUATIC
 MICROORGANISMS. ESTUARY STUDIES ARE INCLUDED AS
 ARE POLLUTION EFFECTS, EXCEPT FOR REPORTS DEALING
 WITH PESTICIDES AND OIL POLLUTION.
 (KEY) ESTUARY STUDIES, POLLUTION EFFECTS
 CODE 77827

AUTH ANONYMOUS
 TITL RESEARCH, JUNE 1977
 PUBL NTIS, US DEPT. OF COMMERCE
 ABST FULLY ANNOTATED BIBLIOGRAPHS PREPARED BY
 INFORMATION SPECIALISTS AT NTIS FROM ITS ON-LINE
 INTERACTIVE BIBLIOGRAPHIC RETRIEVAL SYSTEM.
 (KEY) BIBLIOGRAPHY, RETRIEVAL SYSTEM, ON-LINE
 INTERACTIVE BIBLIOGRAPHIC
 CODE 05107

AUTH ANONYMOUS
 TITL A NUMERICAL MODEL OF DROPLET ENTRAINMENT FROM A
 CONTAINING OIL SLICK
 PUBL USCG, OFFICE OF R + O, REPORT NO. CG-D-05-75
 CODE 04980

AUTH ANONYMOUS
 TITL CLEAN INDUSTRY, ENGINEERING CONSTRUCTION AND
 OPERATIONS
 PUBL GULF PUBLISHING CO.
 ABST NUMEROUS ARTICLES IN VOL. 10, NO. 12 AND VOL. 11,
 NOS. 1, 2, 7, 8, 10, 11 AND 12
 CODE 20407

AUTH ANONYMOUS
 TITL CLEAN MASTER
 PUBL CHARLES KEAR ENTERPRISES INC., 1972
 ABST CATALOG ON OCEANOGRAPHIC EQUIPMENT AND
 INSTRUMENTATION

(KEY) CATALOG, EQUIPMENT, INSTRUMENTATION
 CODE 01730

AUTH ANONYMOUS
 TITL OCEAN PRODUCTS AND LITERATURE
 PUBL OCEAN SCIENCE ON STATION
 CODE 03088

AUTH ANONYMOUS
 TITL OCEAN RESEARCH IN THE 1980S
 PUBL CENTER FOR OCEAN MANAGEMENT STUDIES, URI, AUG.
 1977
 ABST A SERIES OF WORKSHOPS WERE SET UP TO DISCUSS THE
 NEED FOR OCEAN RESEARCH. THESE PAPERS WILL BE USED
 AS A PLANNING TOOL IN THE DEVELOPMENT OF A MAJOR
 RESEARCH PROGRAM FOR THE 1980S.
 (KEY) PHYSICAL, BIOLOGICAL, CHEMICAL, GEOLOGICAL
 CODE 12091

AUTH ANONYMOUS
 TITL OCEANOGRAPHIC OBSERVATIONS AND THEORETICAL
 ANALYSIS OF OIL SLICKS DURING THE GREYHOUND SPILL,
 MARCH 1970
 PUBL LOUISIANA STATE UNIV. AG 716 374
 CODE 02158

AUTH ANONYMOUS
 TITL OFF-LINE CITATION LIST - GENERATED BY DODD III
 S.D.C.'S INTERNATIONAL SEARCH SERVICE
 ABST THIS SEARCH WAS PERFORMED ON POLLUTION
 CODE 25105

AUTH ANONYMOUS
 TITL OREGON'S INDUSTRIAL WASTE TREATMENT RESEARCH
 LABORATORY
 PUBL USEPA
 ABST THIS ARTICLE DISCUSSES THE FACILITY THE EPA IS
 USING TO CONDUCT TESTS AND DEVELOP DEVICES AND
 TECHNIQUES FOR THE CONTROL OF OIL AND HAZARDOUS
 MATERIAL SPILLED IN INLAND AND COASTAL WATERS.
 (KEY) ENVIRONMENTAL SAFETY, CONTROL, HAZARDOUS MATERIALS
 CODE 29227

AUTH ANONYMOUS
 TITL OIL AND DISPERSANTS
 PUBL S.D.C. INTERNATIONAL SEARCH SERVICE, AUG. 6, 1970
 ABST THIS IS AN OFF LINE CITATION LIST.
 (KEY) OIL AND DISPERSANTS
 CODE 21177

AUTH ANONYMOUS
 TITL OIL AND HAZARDOUS MATERIALS, TECHNICAL ASSISTANCE
 DATA SYSTEM
 PUBL EPA, OIL AND SPECIAL MATERIALS CONTROL DIVISION,
 OFFICE OF WATER PROGRAM OPERATIONS
 ABST DESCRIPTION OF THE OIL AND HAZARDOUS MATERIALS,
 TECHNICAL ASSISTANCE DATA SYSTEM AND ITS
 APPLICATIONS TO EMERGENCY SITUATIONS WHERE ON
 SCENE COORDINATION WOULD BE NECESSARY. THE
 ON THE USE OF HAZARD INVOLVED. THE
 COUNTERMEASURES TO BE UTILIZED AND THE PERSONNEL
 SAFETY PRECAUTIONS TO BE TAKEN.
 (KEY) SAFETY PRECAUTIONS, EMERGENCIES, HAZARD,
 COUNTERMEASURES
 CODE 20577

AUTH ANONYMOUS
 TITL OIL AND WATER MIX: PHENOMENON OCCURS WITH CERTAIN
 DETERGENTS
 PUBL COLUMBIA UNIV. OFFICE OF PUBLIC INFO, JAN. 13,
 1973
 ABST DETERGENT FILMS ARE USED IN LABORATORY FOR MIXING
 OIL AND WATER.
 (KEY) DETERGENT FILMS, OIL AND WATER MIXING
 CODE 21308

AUTH ANONYMOUS
 TITL OIL BARRIER STANDARDS, TEST REQUIREMENTS
 PUBL USCG, SSIE NO. 67F-54
 CODE 04428

AUTH ANONYMOUS
 TITL OIL BOOM GEOMETRY
 PUBL UNKNOWN
 ABST GRAPHS SHOWING STEADY STATE OIL BOOM GEOMETRY FROM
 MODEL TESTS, MOORING FIELD, AT VARIOUS CURRENTS.
 CODE 00408

AUTH ANONYMOUS
 TITL OIL BOOMS FOR POLLUTION CONTROL
 PUBL UNIROVAL
 ABST EXPLAINS UNIROVAL'S SEALED BOOM AND GIVES
 SPECIFICATIONS.
 CODE 30388

AUTH ANONYMOUS
 TITL OIL CLEANUP UNDERWAY
 PUBL EVENING BULLETIN, VOL. 681, NO. 72, WED. APRIL 11,
 1973
 ABST ARTICLE DISCUSSES THE OIL SPILL WHEN THE PENNANT
 HIT AN UNDERWATER OBSTRUCTION OFF POPPASQUASH Pt.
 AT RUSTICK BEACH. IT DESCRIBES CLEANUP
 PROCEDURES.
 CODE 30744

AUTH ANONYMOUS

TITLE OIL COMPANIES SPILL AND RUN
PUBL DOLLARS AND SENSE, MONTHLY PUBLICATION, VOL. 24,
FEB. 1977
ABST ARTICLE PERTAINING TO THE ARGO MERCHANT SPILL AND
TANKER TRANSPORT.
KEYW TANKER TRANSPORT, ARGO MERCHANT
CODE 2651F

AUTH ANONYMOUS
TITLE OIL CONTAINMENT METHOD SITED FOR PULL TESTING
PUBL ENVIRONMENTAL CURRENTS, VOL. 4, NO. 12, DEC. 1970
ABST ONE MILLION DOLLAR CONTRACT AWARDED TO
JUNAS-MANVILLE CORP. FROM USCG FOR FURTHER
DEVELOPMENT OF OIL CONTAINMENT SYSTEM FOR OFFSHORE
OIL SPILLS.
CODE 6028A

AUTH ANONYMOUS
TITLE OIL CONTAINMENT SYSTEM
PUBL TEXAS A&M UNIV. FOR USCG, SSIE NO. 67-88226-1
CODE 0443A

AUTH ANONYMOUS
TITLE OIL CONTAINMENT SYSTEMS
PUBL EPA, SURVEILLANCE AND ANALYSIS DIVISION, OCT.
1970, JAN. 1973
ABST THIS REPORT PROVIDES A DESCRIPTION OF VARIOUS OIL
SPILL CONTAINMENT SYSTEMS
KEYW ACCIDENTS AT SEA, NATURAL DISASTERS, RESOURCES
AFFECTED
CODE 0403F

AUTH ANONYMOUS
TITLE OIL CONTAINMENT SYSTEMS
PUBL FEDERAL WATER QUALITY ADMIN., US DEPT. OF THE
INTERIOR
ABST CONTAINMENT SYSTEMS, COMMERCIALY AVAILABLE, AND
UNDER PATENT OR DEVELOPMENT ARE DISCUSSED AND
ILLUSTRATED.
KEYW CONTAINMENT SYSTEMS, PATENTS, DEVELOPMENT
CODE 0040A

AUTH ANONYMOUS
TITLE OIL CONTAINMENT SYSTEMS - CHEMICALLY JELLED BECH.
PUBL ENVIRONMENTAL PROTECTION AGENCY, SSIE NO. 67-12100
CODE 2010P

AUTH ANONYMOUS
TITLE OIL IN THE ARCTIC
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
NO. 66-D-96-79, 4108-2-3
CODE 7058A

AUTH ANONYMOUS
TITLE OIL INDUSTRY DIRECTORY HANDBOOK INDUSTRY
PUBL US DEPT OF THE INTERIOR, GEOLOGICAL SURVEY
ABST LIST OF SELECTED REFERENCES ON OIL SPILLS
CODE 2900P

AUTH ANONYMOUS
TITLE OIL ON THE BEACH STATE ACTION NEEDED
PUBL NEW SCIENCE, LONDON 4817301:480
CODE 1112A

AUTH ANONYMOUS
TITLE OIL ON TROUBLED WATERS
PUBL RESEARCH NEWS, DIV. OF RESEARCH DEVELOPMENT AND
ADMINISTRATION, UNIVERSITY OF MICHIGAN, VOL. XXVII,
NO. 2, AUG. 1975
ABST THIS PAPER DISCUSSES THE PROBLEMS DUE TO OIL
TRANSPORT.
KEYW CLEANUP, PREVENTION, TANKERS
CODE 2535P

AUTH ANONYMOUS
TITLE OIL POLLUTION
PUBL EPA, EDISON WATER QUALITY LAB, OIL POLLUTION
RESEARCH NEWSLETTER, VOL. 14, JULY 1971
CODE 5027A

AUTH ANONYMOUS
TITLE OIL POLLUTION ACT
PUBL 93RD CONGRESS, HR 8917, OCT. 4, 1973
ABST ACT TO BRING OIL POLLUTION ACT, 1961 AS AMENDED,
TO IMPLEMENT 1965 AND 1971 AGREEMENTS IC
INTERNATIONAL CONVENTION FOR PREVENTION OF
POLLUTION OF SEA BY OIL
CODE 6092A

AUTH ANONYMOUS
TITLE OIL POLLUTION ACT AMENDMENTS OF 1973
PUBL REPORT FROM THE COMMITTEE ON MERCHANT MARINE AND
FISHERIES TO ACCOMPANY HR 3451, APRIL 13, 1973,
93RD CONGRESS
CODE 6076A

AUTH ANONYMOUS
TITLE OIL POLLUTION AN INDEX CATALOG TO THE COLLECTION
OF THE OIL SPILL INFORMATION CENTER, VOL. 13,
AUTHOR INDEX
PUBL UNIVERSITY OF CALIFORNIA LIBRARY, 1972
ABST AUTHOR INDEX
KEYW CATALOG, AUTHOR INDEX
CODE 6083B

AUTH ANONYMOUS
TITLE OIL POLLUTION AN INDEX CATALOG TO THE COLLECTION
OF THE OIL SPILL INFORMATION CENTER, VOL. 14
PUBL UNIVERSITY OF CALIFORNIA LIBRARY, 1972
ABST OIL POLLUTION PROBLEMS, MARBONS - 2
KEYW CATALOG
CODE 6081B

AUTH ANONYMOUS
TITLE OIL POLLUTION AT SEA HOW MUCH IS TOO MUCH?
PUBL BIOSCIENCE VOL. 25, 1975
ABST THIS PAPER DISCUSSES THE TOPIC OF LEVELS OF
HYDROCARBONS INPUT INTO THE SEA
KEYW TRANSPORTATION, REFINERIES, INDUSTRIAL
CODE 7127F

AUTH ANONYMOUS
TITLE OIL POLLUTION CONTROL - SPECIAL TECHNIQUES -
BACTERIOLOGICAL DEGRADATION OF OIL SLICKS
PUBL USCG, SSIE NO. 67P-55
CODE 0473A

AUTH ANONYMOUS
TITLE OIL POLLUTION CONTROL AND REQUIREMENTS, VOL. 1
METHODS, VOL. II PLANS
PUBL A.W. LITTLE, INC. AD 690 633
CODE 0167, 0167A

AUTH ANONYMOUS
TITLE OIL POLLUTION CONTROL RESEARCH AND DEVELOPMENT
REQUIREMENTS VOL. 1 - METHODS
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
NO. 74102/002-1
CODE 0168A

AUTH ANONYMOUS
TITLE OIL POLLUTION CONTROL RULES AND REGULATIONS
PUBL RI DEPT. OF HEALTH
ABST STATES THE RULES AND REGULATIONS PREVENTING THE
DISCHARGE OR ESCAPE OF ANY PETROLEUM, GASOLINE,
KEROSENE, TAR, ASPHALT, OIL, OR ANY OTHER PRODUCT
OR MIXTURE THEREOF, INTO THE WATER OF THE STATE OF
RI.
CODE 6023A

AUTH ANONYMOUS
TITLE OIL POLLUTION CONTROL RULES AND REGULATIONS
PUBL RI DEPT. OF HEALTH, 1971
CODE 0022A

AUTH ANONYMOUS
TITLE OIL POLLUTION DETECTION AND SENSING VOLUME 2
PUBL 1976-AUGUST 1978
PUBL RTIS
ABST CITATIONS OF RESEARCH ON SAMPLING, DETECTION AND
CHEMICAL ANALYSIS OF OIL IN WATER ARE PRESENTED.
STUDIES ON REMOTE SENSING PRINCIPALLY USING RADAR,
SLEAM HAVE DAMPING AND INFRARED DETECTION ARE
INCLUDED. THE MAJORITY OF THESE CITATIONS CONCERN
OIL SPILLS, BUT STUDIES ON OIL WASTES, INDUSTRIAL
WASTES, BILGE WATER AND SEWAGE ARE ALSO COVERED.
KEYW OIL SPILLS, CHEMICAL ANALYSIS, DETECTION
CODE 7703 F

AUTH ANONYMOUS
TITLE OIL POLLUTION IN THE SANTA BARBARA CHANNEL
PUBL UNIVERSITY OF CALIFORNIA LIBRARY
ABST A COMPREHENSIVE BIBLIOGRAPHY WITH PARTICULAR
EMPHASIS ON THE OIL SPILL OF JAN. 28, 1965
KEYW PUBLIC RESPONSE, COURT ACTIONS, LEGISLATION, SANTA
BARBARA CHANNEL
CODE 6082D

AUTH ANONYMOUS
TITLE OIL POLLUTION INDEX CATALOG, VOL. III, A - OIL
POLLUTION
PUBL UNIVERSITY OF CALIFORNIA LIBRARY, 1972
ABST AN INDEX CATALOG TO THE COLLECTION OF THE OIL
SPILL INFORMATION CENTER.
KEYW CATALOG, OIL SPILL INFORMATION CENTER
CODE 6080D

AUTH ANONYMOUS
TITLE OIL POLLUTION INDEX CATALOG, VOL. 1
PUBL UNIVERSITY OF CALIFORNIA LIBRARY, 1972
ABST ANONYMOUS ARTICLES
KEYW CATALOG
CODE 6079B

AUTH ANONYMOUS
TITLE OIL POLLUTION OF THE SEA: CLEANUP UP
PUBL MAR. INTL. J., VOL. 10, NO. 2, SPRING 1964
CODE 5027A

AUTH ANONYMOUS
TITLE OIL POLLUTION RESEARCH NEWSLETTER
PUBL EDISON WATER QUALITY LABORATORY, VOL. V, EPA,
SEPT. 1971
ABST OBSERVATIONS AT A LOCAL OIL SPILL AND
EFFECTIVENESS OF CLEANUP OPERATIONS.
KEYW CLEANUP, COLLECTING AGENT, CONTROL
CODE 5082F

AUTH ANONYMOUS
TITLE OIL RETRIEVAL SKIMMER DEVELOPMENT - DAT-4
PUBL USCG, DEC 1971
CODE 0164A

AUTH ANONYMOUS
TITL OIL SLICK ANSWER FROM ICE - TANKER CLEANING AT SEA
PUBL SHIPBUILDING AND SHIPPING RECORD, AUG. 8, 1969
CODE 2133A

AUTH ANONYMOUS
TITL OIL SLICK MOVEMENT - A BIBLIOGRAPHY WITH ABSTRACTS
PUBL APRIL 1976
PUBL DTIC PS-76/0311
ABST THE BIBLIOGRAPHY CITES GOVERNMENT-SPONSORED RESEARCH REPORTS COVERING THE MOVEMENT OF OIL SLICKS IN THE OCEAN. SOME OF THE TOPICS INCLUDE OCEAN CURRENT INTERACTIONS, MODELING OF DRIFT, OCEAN WAVE DISPERSION, AND OCEAN CURRENT STUDIES NEAR VARIOUS COASTS. (CONTAINS 35 ABSTRACTS)
KEYW OIL SPILLS, OCEAN CURRENT INTERACTIONS, MODELING OF DRIFT
CODE 7741F

AUTH ANONYMOUS
TITL OIL SLICK SURVEILLANCE AND FORECASTING, SLICK THICKNESS MEASURING DEVICE
PUBL USCG, NO. 12130; SSIE NO. 67-12130
CODE 0434A

AUTH ANONYMOUS
TITL OIL SLICKS AND FILMS
PUBL DEFENSE DOCUMENTATION CENTER, JAN. 1953-MAY, 1971. REPORT DATED 3/72 NO. DD-145-71-04
ABST REFERENCES PERTAINING TO THE CLEANING AND REMOVAL OF OIL SLICKS, OIL FILMS, AND RELATED FILMS FROM SEA SURFACES, OR WATER SURFACES HAVE BEEN COMPILED IN THIS BIBLIOGRAPHY.
KEYW CLEANUP, REMOVAL, BIBLIOGRAPHY
CODE 5044F

AUTH ANONYMOUS
TITL OIL SPILL RECOVERY VESSEL
PUBL NETHERLANDS PATENT NL 7315-128, JUNE 20-1974
ABST OIL FLOATING ON WATER IS RECOVERED USING A VESSEL WITH A CYCLONE CHAMBER INTO WHICH A SKIMMED LAYER IS ADMITTED VIA A LATERAL OPENING, ONE EDGE OF WHICH IS DEFINED BY AN ADJUSTABLE SKIMMER, THE INFLUX TO THE CHAMBER BODY SOLELY DEPENDENT ON THE TRANSLATERAL SPEED OF THE VESSEL.
CODE 3130A

AUTH ANONYMOUS
TITL OIL SPILL - SANTA BARBARA
PUBL UNIV. OF CAL. DEPT. OF BIOLOGICAL SCIENCE, FEB. 1971
ABST SHORT TERM ANALYSIS OF MACROPLANKTON AND FISH FROM SANTA BARBARA OIL SPILL.
CODE 6052A

AUTH ANONYMOUS
TITL OIL SPILL AND OIL POLLUTION REPORTS, JULY 1974 - OCT. 1974
PUBL EPA, NO. EPA 670/2-75-003
CODE 6008A

AUTH ANONYMOUS
TITL OIL SPILL AND POLLUTION NEWS ARTICLES
PUBL UNKNOWN
ABST VARIOUS NEWSPAPER ARTICLES
KEYW NEWS ARTICLES, OIL SPILLS, POLLUTION
CODE 01810

AUTH ANONYMOUS
TITL OIL SPILL BARRIERS
PUBL MINUTES OF THE ASTM COMMITTEE, JAN. 23, 1976
ABST MINUTES OF PROPOSED ASTM COMMITTEE.
KEYW OIL SPILL, OPERATION, DISCUSSION
CODE 2913F

AUTH ANONYMOUS
TITL OIL SPILL CONFERENCE
PUBL API, OIL SPILL CONFERENCE, MARCH 8, 1977
ABST PROCEEDING OF THE OIL SPILL CONFERENCE, NEW ORLEANS, LA.
KEYW PROCEEDINGS, CONFERENCE, OIL SPILL
CODE 0041B

AUTH ANONYMOUS
TITL OIL SPILL CONTAINMENT
PUBL USAP FOR USCG, SSIE NO. 62-62-65
CODE 0443A

AUTH ANONYMOUS
TITL OIL SPILL CONTAINMENT SYSTEMS
PUBL EPA, JAN. 1973
ABST THIS REPORT DESCRIBES VARIOUS OIL SPILL CONTAINMENT SYSTEMS. INCLUDES CONCEPTUAL DESIGN, SYSTEMS UNDER PATENT, SYSTEMS IN STAGES OF FINAL DEVELOPMENT, AND VARIOUS FULL SCALE COMMERCIAL EQUIPMENT AVAILABLE TODAY.
KEYW CONTAINMENT, DESIGN, CONSTRUCTION
CODE 0031B

AUTH ANONYMOUS
TITL OIL SPILL DETECTION
PUBL US EPA AND USCG SSIE NO. 62-3016A-1
CODE 0432A

AUTH ANONYMOUS
TITL OIL SPILL DRIFT CAUSED BY THE COMBINED EFFECTS OF WIND AND WAVES
PUBL UNIV. OF MISSOURI, OCT. 1973. AD 777 702
CODE 0219A

AUTH ANONYMOUS
TITL OIL SPILL FIGHTER ADMINISTERING THE OCEAN DUMPING ACT
PUBL UNKNOWN
ABST THIS PAPER DISCUSSES KENNETH BIGLANE'S ROLE IN COPING WITH OIL SPILLS, THE OCEAN DUMPING ACT, FORMALLY KNOWN AS THE MARINE POLLUTION RESEARCH AND SANCTUARIES ACT, GIVES EPA THE RESPONSIBILITY FOR REGULATING THE DUMPING OF ALL MATERIALS EXCEPT BULKED MATERIALS.
KEYW OCEAN DUMPING ACT, REGULATING, DUMPING OF MATERIALS
CODE T851AF

AUTH ANONYMOUS
TITL OIL SPILL SPOILER
PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY, 1974
CODE 0372A

AUTH ANONYMOUS
TITL OIL SPILL TREATING AGENTS - A COMPENDIUM
PUBL PACIFIC NORTHWEST LAB. CONTRACT NO. 21200003, MAY 1970
ABST A SINGLE SOURCE COMPENDIUM OF INFORMATION ON AVAILABLE OIL SPILL TREATING AGENTS AS AN INITIAL BASIS OF SELECTION OF TREATING AGENTS. THIS VOLUME IS INTENDED TO AID IN LOGISTIC PLANNING BY INDICATING THE QUANTITIES AND LOCATIONS OF WAREHOUSED MATERIALS AND POTENTIAL PRODUCTION SITES.
KEYW TREATING AGENTS, LOGISTIC PLANNING, WAREHOUSED MATERIALS
CODE 0024A

AUTH ANONYMOUS
TITL OIL SPILL TREATING AGENTS SELECTION BASED ON ENVIRONMENTAL FACTORS
PUBL ARTHUR D. LITTLE, INC., OCT. 1970
ABST A CROSS-SECTION OF ENVIRONMENTAL CHARACTERISTICS REPRESENTATIVE OF CONDITIONS ALONG THE US COASTLINES AND INLAND WATERWAYS, SPECIFICALLY, WHICH CHARACTERISTICS ARE IMPORTANT AND HOW THEY INFLUENCE OIL SPILL TREATING AGENTS AND TECHNIQUES
KEYW TREATING AGENTS, CONDITIONS, CHARACTERISTICS
CODE 0042A

AUTH ANONYMOUS
TITL OIL SPILL TREATING AGENTS TEST PROCEDURES: STATUS AND RECOMMENDATIONS
PUBL BATTELLE MEMORIAL INSTITUTE, PACIFIC NORTHWEST LAB. MAY 15, 1970
ABST EXISTING EFFECTIVENESS AND TOXICITY MEASUREMENT METHODS ARE ASSESSED. IT IS ALSO TO BE DETERMINED WHETHER ANY COMBINATION OF EXISTING BIOASSAY TECHNIQUES WILL ADEQUATELY MEASURE THE TOXICITY OF THE TREATING AGENTS.
KEYW TREATING AGENTS, TOXICITY, BIOASSAY TECHNIQUES
CODE 0043A

AUTH ANONYMOUS
TITL OIL SPILL, LONG ISLAND SOUND, MARCH 23, 1972. ENVIRONMENTAL EFFECTS
PUBL OIL AND HAZARDOUS MATERIALS PROGRAM SERIES, JAN. 1973, EPA NO. 60-01-004A
ABST THIS STUDY WAS PRINCIPALLY UNDERTAKEN TO DETERMINE THE EFFECTS OF A NO. 2 FUEL OIL ON THE ENVIRONMENT.
KEYW SEDIMENTS, NO. 2 FUEL OIL, MORTALITY RATES
CODE 0152H

AUTH ANONYMOUS
TITL OIL SPILLAGE STUDY - LITERATURE SEARCH AND CRITICAL EVALUATION FOR SELECTION OF PROMISING TECHNIQUES TO CONTROL AND PREVENT DAMAGE
PUBL USCG, DEPT. OF TRANSPORTATION, REPORT NO. AD 780442, ONP-319, JUNE, 1967
ABST THIS REPORT DISCUSSES POLLUTION OF LARGE EXPANSES OF OCEAN OIL TO TANKERS, OPERATIONAL PRACTICES, TRAFFIC DENSITY AND HUMAN FAILINGS.
KEYW CONTROL, PREVENTION, REMOVAL, RECOVERY, CLEANUP, TANKERS
CODE 2913F

AUTH ANONYMOUS
TITL OIL SPILLAGE STUDY LITERATURE SEARCH AND CRITICAL EVALUATION FOR SELECTION OF PROMISING TECHNIQUES TO CONTROL AND PREVENT DAMAGE
PUBL USCG, DEPT. OF TRANSPORTATION, BATTELLE MEMORIAL INSTITUTE, REPORT NO. TCU-1550-A, NOV. 1967
ABST THE PURPOSE OF THIS REPORT IS TO PROVIDE REVIEW AND EVALUATION OF CURRENT TECHNOLOGY OF PREVENTION AND CONTROL OF SPILLS, RESTORATION OF SHORE AND WATER FOWL, AND EFFECTS ON AQUATIC LIFE. OBJECT OF THE STUDY IS TO ASSIST IN ESTABLISHING PROCEDURES FOR CONTROL AND CLEANUP AND IMPROVED CAPABILITY FOR PREVENTION.
KEYW RECOVERY, CLEANUP, CONTROL, PREVENTION
CODE 4018B

AUTH ANONYMOUS
TITL OIL SPILLS AND SPILLS OF HAZARDOUS SUBSTANCES
PUBL OIL AND SPECIAL MATERIALS CONTROL DIVISION, OFFICE

- OF WATER POLLUTION OPERATIONS; EPA, MARCH 1977
 ABST THIS PUBLICATION IS EFFECTIVE IN DESCRIBING SOME
 OF THE MORE SIGNIFICANT SPILL INCIDENTS AND THE
 MECHANISMS TO DEAL WITH THEM.
 KEYW PROTECTION, PREVENTION, RESTORE ENVIRONMENTAL
 IMPACT
 CODE 0203
- AUTH ANONYMOUS
 TITL OIL SPILLS AT SEA
 PUBL UNKNOWN
 ABST PHOTOGRAPHS ILLUSTRATING SOME OF THE CONSEQUENCES
 OF ACCIDENTS INVOLVING OIL.
 KEYW ACCIDENTS, CONSEQUENCES
 CODE 7351
- AUTH ANONYMOUS
 TITL OIL SPILLS: PROBLEMS AND OPPORTUNITIES
 PUBL INT/MARINE INDUSTRY COLLEGIUM, OPPORTUNITY SPIFF,
 INT SEA GRANT PROGRAM NO. 9, WORKING DRAFT 4/22/77
 ABST THIS IS A WORKING DRAFT WHICH TOUCHES THE PROBLEMS
 INVOLVED IN OIL SPILLS.
 KEYW CLEANUP, PREVENTION, PANACEA
 CODE 0150
- AUTH ANONYMOUS
 TITL OIL TAGGING SYSTEM STUDY
 PUBL FEDERAL WATER POLLUTION CONTROL ADMIN., DEPT. OF
 THE INTERIOR, MAY 1976
 ABST SEVERAL METHODS OF IDENTIFYING THE SOURCE OF OIL
 POLLUTION ARE CRITICALLY REVIEWED.
 KEYW IDENTIFICATION, SOURCES, TAGGING SYSTEM
 CODE 0030
- AUTH ANONYMOUS
 TITL OIL WATER SEPARATORS, A BIBLIOGRAPHY WITH
 ABSTRACTS
 PUBL US DEPT. OF COMMERCE, NTIS, SPRINGFIELD VA
 CODE 0317
- AUTH ANONYMOUS
 TITL OIL-WATER DETECTOR
 PUBL MULTINATIONAL, MODEL 1475
 ABST THE ELECTRONIC OIL DETECTOR CONSISTS OF A SENSER
 DEVICE SUSPENDED BETWEEN PONTOONS, CONNECTED BY A
 WIRE TO A CONTROL BOX ON SHORE. IT CAN DETECT OIL
 ON THE WATER IN VERY SMALL QUANTITIES BY MEASURING
 THE REFRACTIVE INDEX OF WATER. THE MANUAL GIVES
 SPECIFICS.
 CODE 3055
- AUTH ANONYMOUS
 TITL OPERATION, ORGANIZATIONAL, DIRECT AND GENERAL
 SUPPORT AND DEPOT MAINTENANCE MANUAL REPAIR PARTS
 PUBL REC INDUSTRIES, CINCINNATI OH
 ABST THIS MANUAL IS PUBLISHED FOR THE USE OF THE
 PERSONNEL OF REC INDUSTRIES INC. PROVIDES
 INFORMATION ON OPERATION, MAINTENANCE,
 ACCESSORIES, COMPONENTS AND ATTACHMENTS.
 KEYW OPERATION, MAINTENANCE, ACCESSORIES
 CODE 7008
- AUTH ANONYMOUS
 TITL OPTICAL RANGING SENSING OF OIL SLICKS: SIGNATURES
 ANALYSIS AND SYSTEMS EVALUATION
 PUBL UNIV. OF MICH. OCT. 1971
 CODE 0200
- AUTH ANONYMOUS
 TITL OUR DIRTY WATER
 PUBL PROVIDENCE SUNRAY JOURNAL, PROVIDENCE JOURNAL AND
 EVENING BULLETIN, OCT. 1971
 ABST A WELL LONG EXAMINATION OF R.I.'S WATER POLLUTION
 CONTROL PROGRAM.
 KEYW SEWAGE TREATMENT, SHELLFISHING, TOXICITY
 CODE 4030
- AUTH ANONYMOUS
 TITL PART THREE COST ANALYSIS
 PUBL COMBATING POLLUTION BY OIL SPILLS, VOL. 1
 METHODS, ARTHUR D. LITTLE, INC., AC 00635, JUNE
 1969, REPORT TO THE DEPARTMENT OF TRANSPORTATION
 THIS REPORT DISCUSSES COSTS ASSOCIATED WITH
 COMBATANT METHODS.
 KEYW MATERIAL, OPERATION COSTS, CAPITAL COSTS
 CODE 7135
- AUTH ANONYMOUS
 TITL PARTICLE VACUUM ACCELERATED GRAVITY CONCEPT
 PUBL BEMERICKS RESEARCH INC. FOR COAST GUARD
 CODE 0350
- AUTH ANONYMOUS
 TITL PARTICLE VACUUM ACCELERATED GRAVITY CONCEPT
 PUBL BEMERICKS RESEARCH INC., 5516 N.W. 62-24
 CODE 0452
- AUTH ANONYMOUS
 TITL PERFORM A SCIENTIFIC STUDY TO DETERMINE THE LEANAY
 OF OIL SLICKS UNDER VARIOUS WINDS AND SEAS
 PUBL USCG, MD-66-83, 107-0, MARCH 19, 1973
 CODE 2060
- AUTH ANONYMOUS
 TITL PERFORMANCE EVALUATION OF AN OIL CONTAINMENT
 DAMPER SERIAL DELIVERY SYSTEM
- PUBL USCG, OFFICE OF R + D, REPORT NO. 73-102-5/8, JAN.
 1974
 CODE 0493
- AUTH ANONYMOUS
 TITL PETROLEUM IN THE MARINE ENVIRONMENT
 PUBL WORKSHOP ON INPUTS, PATES, AND THE EFFECTS OF
 PETROLEUM IN THE MARINE ENVIRONMENT, OCEAN AFFAIRS
 BOARD, NATIONAL ACADEMY OF SCIENCES, MAY 21, 1973
 ABST PRIMARY CONCERN OF THE WORKSHOP WAS TO EVALUATE
 EXISTING INFORMATION RATHER THAN DEVELOP NEW
 RESEARCH.
 KEYW PETROLEUM INPUTS, PATES, EFFECTS
 CODE 4030
- AUTH ANONYMOUS
 TITL PHOTOGRAPHIC DETECTION OF SHIP-GENERATED OIL
 SLICKS
 PUBL USCG(DAT-4)
 CODE 0210
- AUTH ANONYMOUS
 TITL PHYSICAL AND CHEMICAL BEHAVIOR OF CRUDE OIL SLICKS
 ON THE WATER
 PUBL JBP SCIENTIFIC CORP., PUBLICATION NO. 4290, APRIL
 30, 1976, PHOTOGRAPHS
 ABST FOUR SMALL RESEARCH OIL SPILLS WERE MADE IN THE
 NO. ATLANTIC TO DETERMINE THE PHYSICAL AND
 CHEMICAL BEHAVIOR OF FRESH OIL SLICKS ON THE OPEN
 OCEAN. EACH SPILL WAS MADE FROM A RESEARCH VESSEL
 AND THEN WAS TRACKED BY VESSEL AND AIRCRAFT FOR UP
 TO TWO DAYS. TWO CRUDE OILS WERE USED, AND EACH
 EXPERIENCED DIFFERENT SEA CONDITIONS.
 KEYW RESEARCH OIL SPILLS, PHYSICAL AND CHEMICAL
 BEHAVIOR, TRACKING
 CODE 7672 (ORIGINAL PHOTOS WITH C. BROWN, 310 PASTORE
 HALL)
- AUTH ANONYMOUS
 TITL PHYSICAL PROCESS IN THE SPREAD OF OIL ON A WATER
 SURFACE
 PUBL INT, AD 754 261
 CODE 0190
- AUTH ANONYMOUS
 TITL POLLUTING INCIDENTS IN AND AROUND US WATERS
 1971-1973
 PUBL USCG, DEPT. OF TRANSPORTATION
 ABST FOUR PAPERS WHICH LIST POLLUTING INCIDENTS
 ACCORDING TO WHERE, HOW MUCH, WHAT TYPE, ETC. OF
 OIL SPILLS.
 CODE 3140
- AUTH ANONYMOUS
 TITL POLLUTION INCIDENTS IN AROUND US WATERS, CALENDAR
 YEARS 1971, 1972, 1973
 PUBL USCG, DEPT. OF TRANSPORTATION
 ABST THESE REPORTS CONTAIN STATISTICS MAINTAINED BY THE
 COAST GUARD REPRESENTING DISCHARGES MADE IN THE US
 NAVIGABLE WATERS.
 KEYW STATISTICS, DISCHARGES, EFFECTS, US NAVIGABLE
 WATERS
 CODE 0171
- AUTH ANONYMOUS
 TITL PUMP OF NEW BEDFORD, OFFSHORE OIL AND GAS
 PUBL MAYORS COMMITTEE ON OFFSHORE OIL, NEW BEDFORD
 PLANNING DEPT.
 ABST MAPS AND INFORMATION OF THE PUMP AT NEW BEDFORD.
 CODE 2003
- AUTH ANONYMOUS
 TITL POTENTIAL OIL POLLUTION INCIDENTS FROM OIL AND GAS
 WELL ACTIVITIES IN LAKE ERIE - THEIR PREVENTION
 AND CONTROL
 PUBL INTERNATIONAL LAKE ERIE WATER POLLUTION BOARD,
 SEPT. 1969
 ABST THE REPORT DETERMINES THE ADEQUACY OF DRILLING
 OPERATIONS, CLEAN UP METHODS, AND CONTINGENT
 PLANS TO CONFINE, REMOVE AND PREVENT OIL POLLUTION
 ON LAKE ERIE.
 KEYW DRILLING, CLEAN UP, CONTINGENCY, PREVENTION,
 REMOVAL, CONFINEMENT
 CODE 0150
- AUTH ANONYMOUS
 TITL PRELIMINARY GUIDE- FORECASTING OIL SLICK BEHAVIOR
 PUBL USCG, JULY 1971, AD 762 350
 CODE 0190
- AUTH ANONYMOUS
 TITL PRELIMINARY PHYSICAL IMPACTS OF OFF-SHORE PETROLEUM
 DEVELOPMENTS
 PUBL INT SEA GRANT PUBLICATION, NTIS 76-20
 CODE 0350
- AUTH ANONYMOUS
 TITL PRELIMINARY REPORT - ENVIRONMENTAL ASSESSMENT OF
 TREATED VERSUS UNTREATED OIL SPILLS
 PUBL COLLEGE OF ENGINEERING, DUS PROJECT, MARCH 1977
 ABST A DRAFT COPY OF THE ABOVE.
 KEYW TREATED SPILLS, ENVIRONMENTAL ASSESSMENT
 CODE REF.
- AUTH ANONYMOUS
 TITL PRELIMINARY REPORT, THE GULF REALMANT OIL SPILL

- PUBL US DEPT. OF COMMERCE, NATIONAL OCEANIC AND ATMOSPHERIC ADMINISTRATION
 ABST THIS IS A PRELIMINARY SCIENTIFIC REPORT CONTAINING A SUMMARY FACT SHEET REGARDING THE ANGO MERCHANT SPILL.
 KEYW ANGO MERCHANT, SUMMARY FACT SHEET, SCIENTIFIC REPORT, OIL SPILL
 CODL 0149F
- AUTH ANONYMOUS
 TITL PREVENTION AND CONTROL OF MARINE OIL POLLUTION REGIONAL MARINE OIL POLLUTION CONFERENCE-AUSTRALIA NOVEMBER 8-10, 1976
 PUBL NATIONAL LIBRARY OF AUSTRALIA
 ABST PAPERS PRESENTED: OIL POLLUTION OF THE SEA-THE WORLDWIDE SLENL; TANKER SAFETY AND THE ENVIRONMENT; OFFSHORE ACTIVITIES AND THE ENVIRONMENT; OIL SPILL CLEANUP; APPLICATION OF EQUIPMENT AND METHODS; THE CURRENT STATE OF OIL POLLUTION PREVENTION AND CONTROL IN THE US AND CANADA; THE SITUATION IN JAPAN; MARINE OIL POLLUTION LEGISLATION-WESTERN EUROPE; EVALUATION OF THE ENVIRONMENTAL IMPLICATIONS OF OIL SPILL DISPERSANTS; EFFECTS OF OIL ON THE MARINE ENVIRONMENT; MARINE POLLUTION-LEGAL AND FINANCIAL ASPECTS.
 KEYW OIL SPILL, PREVENTION, DISPERSANTS, OFFSHORE
 CODL 7709 F
- AUTH ANONYMOUS
 TITL PREVENTION AND CONTROL OF OIL SPILLS
 PUBL AMERICAN PETROLEUM INSTITUTE LIBRARY OF CONGRESS LATAJGG NL. 74-127324
 ABST PROCEEDINGS OF JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS. JUNE 1971, 1971 SHEARSON RAND HUSSELL WASHINGTON, D.C.
 KEYW OIL SPILL, PREVENTION, CONTROL
 CODL 7718
- AUTH ANONYMOUS
 TITL PREVENTION AND CONTROL OF OIL SPILLS
 PUBL API, EPA, USCG, PROCEEDINGS OF JOINT CONFERENCE, JUNE 1971
 ABST COMPREHENSIVE STUDY OF ALL SUBJECTS
 CODL 8005F
- AUTH ANONYMOUS
 TITL PRIMARY PHYSICAL IMPACT OF OFFSHORE PETROLEUM DEVELOPMENTS
 PUBL NOAA, MISSI 74-20, APRIL 1974, COM 74-11775
 ABST THESE STUDIES ON THE INITIAL PHYSICAL EFFECTS OF OFFSHORE OIL DEVELOPMENT RESPOND TO THE NEED FOR INFORMATION ON POTENTIAL PETROLEUM PRODUCTION FROM THE ATLANTIC AND GULF OF ALABAMA CONTINENTAL SHELVES.
 KEYW CONTINENTAL SHELVES, WEATHERING, EVAPORATION, DIFFUSION
 CODL 8028
- AUTH ANONYMOUS
 TITL PROBABLE BEHAVIOR AND FATE OF A WINTER OIL SPILL IN THE BEaufort SEA
 PUBL TECHNOLOGICAL DEVELOPMENT REPORT NO. EPS-NOEL-71-3, ENVIRONMENTAL IMPACT CONTROL DIRECTORATE, AUG. 1978
 KEYW DYNAMIC ICE, TRANSITION ZONE, MOVING ICE SHEET, BEAUFORT SEA
 CODL 7141F
- AUTH ANONYMOUS
 TITL PROCEEDING FROM THE THIRTEENTH COASTAL ENGINEERING CONFERENCE
 PUBL NATIONAL RESEARCH COUNCIL OF CANADA
 ABST A DISCUSSION OF SOME MEASURED WAVE DATA HEIGHT AND PEAK PERIODS OF MEASURED WAVES IN OCEAN OFF WESTERN HEAD, NOVA SCOTIA ARE COMPARED TO PARAMETER DERIVED FROM INDIVIDUAL WAVE HEIGHTS AND BY TUCKER METHOD.
 CODL 8001F
- AUTH ANONYMOUS
 TITL PROCEEDINGS
 PUBL JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS API, PMPCA, DEC. 1969
 ABST OBJECTIVES WERE TO OUTLINE OVERALL DIMEN. OF OIL SPILL PROBLEMS, EMPLOYE THE PRESENT STATE OF THE ART OF PREVENTION AND CONTROL OF OIL SPILLS, REVIEW OF THE RELEVANT RESEARCH AND DEVELOPMENT EFFORTS OF GOVERNMENT AND PRIVATE INDUSTRY.
 KEYW OIL SPILL, PREVENTION, CONTROL
 CODL 8011F
- AUTH ANONYMOUS
 TITL PROCEEDINGS OF A WORKSHOP ON ENVIRONMENTAL OCEANOGRAPHY OF THE GULF OF MEXICO
 PUBL DEPARTMENT OF OCEANOGRAPHY, TEXAS A & M UNIVERSITY
 ABST THE AID OF THE WORKSHOP WAS TO DEFINE THE MOST CRITICAL ENERGY-RELATED ENVIRONMENTAL PROBLEMS IN THE GULF OF MEXICO AND DEVELOP THE FRAMEWORK FOR A PROGRAM OF RESEARCH TO SOLVE THESE PROBLEMS.
 KEYW ENERGY RELATED ENVIRONMENTAL PROBLEMS, RESEARCH, SOURCES OF ENERGY
 CODL 2678F
- AUTH ANONYMOUS
 TITL PROCEEDINGS OF ECOLOGICAL DAMAGE ASSESSMENT CONFERENCE NOV. 12-14, 1970
 PUBL SOCIETY OF PETROLEUM INDUSTRY BIOLOGISTS
 ABST THE OBJECTIVE OF THIS CONFERENCE ON ECOLOGICAL DAMAGE ASSESSMENT IS TO BRING TOGETHER SCIENTISTS FROM GOVERNMENT, INDUSTRY AND UNIVERSITIES TO EXPLORE THE STATE-OF-THE-ART IN ECOLOGICAL DAMAGE ASSESSMENT.
 KEYW ECOLOGICAL DAMAGE ASSESSMENT, OIL SPILL
 CODL 7779F
- AUTH ANONYMOUS
 TITL PROCEEDINGS OF JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS
 PUBL API, EPA, USCG, WASHDC 13-15, 1973
 ABST VARIOUS ARTICLES REGARDING: PREVENTION, IDENTIFICATION OF OIL, CONTROL, TECHNOLOGY, APPLIED CONTROL TECHNOLOGY AND BIOLOGICAL EFFECTS OF OIL SPILLS.
 KEYW PREVENTION, IDENTIFICATION, TECHNOLOGY, BIOLOGICAL EFFECTS.
 CODL 8002B
- AUTH ANONYMOUS
 TITL PROCEEDINGS OF THE INTERNATIONAL CONFERENCE ON WASTE OIL RECOVERY AND REUSE FEBRUARY 12-14, 1974
 PUBL ASSOCIATION OF PETROLEUM REFINERS
 ABST OIL REUSE, WASTE OIL; CHARACTERISTICS AND USE AS A PUBL
 KEYW WASTE OIL RECOVERY, MANAGEMENT, OIL SPILL
 CODL 7788F
- AUTH ANONYMOUS
 TITL PROCEEDINGS ON A WORKSHOP ON THE PHYSICAL BEHAVIOR OF OIL IN THE MARINE ENVIRONMENT HELD IN PRINCETON, NEW JERSEY MAY 8-9, 1974
 PUBL DEPARTMENT OF CIVIL ENGINEERING PRINCETON UNIVERSITY
 ABST THE OBJECTIVE OF THE WORKSHOP IS TO EXAMINE CRITICALLY CURRENT KNOWLEDGE OF THE SUBJECT OF BRINGING TOGETHER FIFTY SCIENTISTS IN RELATED FIELDS OF RESEARCH. THE TWO DAYS OF INVITED PAPERS WERE DEVOTED TO THE EXAMINATION OF SIX AREAS INVOLVED WITH UNDERSTANDING THE PHYSICAL BEHAVIOR OF OIL.
 KEYW OIL SPILL FORECASTING, MODELLING, ENTRAINMENT.
 CODL 7780F
- AUTH ANONYMOUS
 TITL PROCEEDINGS: INDUSTRY-GOVERNMENT SEMINAR OIL SPILL TREATING AGENTS, APRIL 8-9, 1970, WASHINGTON, D.C.
 PUBL API COMMITTEE FOR AIR AND WATER CONSERVATION AND US DEPT. OF THE INTERIOR
 ABST MAJOR OBJECTIVE: TO ARRANGE FOR A FORUM WHERE THE GUIDELINES FOR SAFE AND EFFECTIVE USE OF OIL SPILL TREATING AGENTS COULD BE CONSIDERED.
 KEYW TREATING AGENTS, GUIDELINES FOR SAFETY, EFFECTIVE USE
 CODL 8002A
- AUTH ANONYMOUS
 TITL PROCEEDINGS: JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS
 PUBL API - PMPCA, DEC. 15-17, 1969
 ABST THE OBJECTIVE OF THE CONFERENCE WAS TO DEBATE THE OVERALL DIMENSIONS OF THE OIL SPILLS PROBLEM, EXPLORE THE PRESENT STATE OF THE ART OF PREVENTION AND CONTROL AND REVIEW RELEVANT RESEARCH AND DEVELOPMENT EFFORTS.
 KEYW FLUID DYNAMICS, DISPERSANTS, TOXICITIES
 CODL 8001B
- AUTH ANONYMOUS
 TITL PRODUCT INFORMATION SHEET
 PUBL UNKNOWN
 ABST DISPERSANTS
 KEYW DISPERSANTS
 CODL 2675F
- AUTH ANONYMOUS
 TITL PROJECTS
 PUBL WILKINSON MATERIAL SPILLS RESEARCH NEWSLETTER, VOL. 1, MAY 1971
 ABST GIVES NEW PROJECTS PROPOSALS, DESCRIBES COMPLETION OF VARIOUS PROJECTS AND GENERAL INFORMATION ON RECENT OIL SPILLS.
 CODL 3063B
- AUTH ANONYMOUS
 TITL PROTOTYPE HIGH SEAS OIL RECOVERY SYSTEM PHASE I
 PUBL SYSTEM DEVELOPMENT - LOCKHEED MISSILES AND SPACE CO., FEB. 1972, AD 758 351, AD 758 352, AD 758 353
 CODL 0185F
- AUTH ANONYMOUS
 TITL PUBLICATION AND MATERIALS
 PUBL API
 ABST CATALOG
 CODL 2623F
- AUTH ANONYMOUS
 TITL PUBLICATION LIST FOR UNIVERSITIES
 PUBL GENERAL ELECTRIC
 ABST PUBLICATIONS PREPARED BY G.E.
 CODL 2568F

AUTH ANONYMOUS
 TITLE RADAR IMAGERY OF OIL SLICKS
 PUBL IEEE TRANSACTIONS ON AEROSPACE AND ELECTRONIC SYSTEMS, VOL. AES-9 SEPT. 1973

AUTH ANONYMOUS
 TITLE RADAR IMAGERY OF OIL SLICKS
 PUBL IEEE TRANSACTIONS ON AEROSPACE AND ELECTRONIC SYSTEMS, VOL. AES-9, SEPT. 73, 630-634 PP
 REYN RADAR, OIL SLICK
 CODE 0398R

AUTH ANONYMOUS
 TITLE RECENT OIL SPILLS
 PUBL OIL AND HAZARDOUS MATERIALS RESEARCH NEWSLETTER, VOL. 1, JAN. 1970
 ABST DISCUSSES THE MEXO OIL SPILL AND THE GROUNDING OF THE BARGE FLORIDA.
 CODE 3059R

AUTH ANONYMOUS
 TITLE RECOVERY OF FLOATING OIL ROTATING DISK TYPE SWIMMER
 PUBL ATLANTIC RESEARCH SYSTEMS DIVISION, MARINE SYSTEMS, A DIVISION OF THE SUGUEMAMA CORP., COSTA MESA, CA FOR EPA, JULY 1971
 ABST LAB. TESTS OF DISC MATERIALS IN OILS RANGING FROM LIGHT DIESEL TO BUNKER C, INDICATING THAT ALUMINUM WAS BEST MATERIAL. EXPERIMENTAL TESTS ON MODEL DISCS IN STILL WATER ESTABLISHED BASELINE PERFORMANCE DATA AND UNDERSTANDING OF SCALING EFFECTS. ALSO SHOWED THAT VELOCITY VECTOR IN THE FLUID SHOULD BE IN THE SAME DIRECTION AS THE CURRENT FLOW.
 REYN RECOVERY, ROTATING DISK, SWIMMERS
 CODE 0004R

AUTH ANONYMOUS
 TITLE RECOVERY OF OIL SPILLS USING VORTEX ASSISTED RECOVERY SYSTEM
 PUBL EPA, PROJECT NO. 15080DJ, CONTRACT NO. 14-12-513, JULY, 1970
 ABST STUDIES WERE CONDUCTED TO DETERMINE THE FEASIBILITY OF A CONCEPT FOR RECOVERY OF FLOATING OIL SLICKS WHICH UTILIZES A PUMP INDUCED VORTEX AND A VACUUM SUCTION OF GOANDA NOZZLE.
 REYN RECOVERY, PUMP INDUCED VORTEX, VACUUM SUCTION, GOANDA NOZZLE
 CODE 0053R

AUTH ANONYMOUS
 TITLE RECYCLED OIL... A QUESTION OF QUALITY
 PUBL OHS, STANDARD VOL. 21, NOV. 24 - DEC. 1, 1970
 ABST THIS REPORT DISCUSSES THE REUSE OF WASTED OIL.
 REYN RECYCLING OIL, CONSUMPTION REDUCTION, HAZARDOUS REDUCTION
 CODE 2934F

AUTH ANONYMOUS
 TITLE REGULATION FOR VESSEL TO VESSEL TRANSFER OF PETROLEUM PRODUCTS
 PUBL COASTAL RESOURCES MANAGEMENT COUNCIL, GENERAL LAWS OF RI, AUG. 1972
 ABST A STATEMENT OF MINIMUM REQUIREMENTS OF PROCEDURES TO BE FOLLOWED DURING TRANSFER OF PETROLEUM AND PETROLEUM PRODUCTS FROM VESSEL TO VESSEL IN CALL TO INSURE THAT SUCH TRANSFERS ARE CARRIED OUT IN A MANNER WHICH WILL NOT HARM MARINE ENVIRONMENT OF THIS STATE.
 REYN PETROLEUM TRANSFER
 CODE 6043R

AUTH ANONYMOUS
 TITLE REGULATIONS FOR US TANK VESSELS CARRYING OIL IN FOREIGN TRADE AND FOREIGN TANK VESSELS THAT ENTER THE NAVIGABLE WATER OF THE US.
 PUBL DEPT. OF TRANSPORTATION, USCG
 CODE 7512R

AUTH ANONYMOUS
 TITLE REMOTE SAMPLER FOR DETERMINING RESIDUAL OIL CONTENTS OF SURFACE WATER
 PUBL NAVAL SHIP RESEARCH AND DEVELOPMENT CENTER, INC., 1972, AD 74C 217
 CODE 0217R

AUTH ANONYMOUS
 TITLE THE REMOTE SENSING OF OIL SLICKS BY RADAR
 PUBL NAVAL RESEARCH LAB., AD 709 987
 CODE 0212R

AUTH ANONYMOUS
 TITLE REMOTE SENSING OF SOUTHERN CALIFORNIA OIL POLLUTION EXPERIMENT
 PUBL USCG, DAT-6, PB 203 194, JULY 1971
 CODE 0203R

AUTH ANONYMOUS
 TITLE REMOTE SENSING OIL POLLUTION SYSTEM CONCEPT-EVALUATION
 PUBL USCG DAT-6, JUNE 1971
 CODE 0207R

AUTH ANONYMOUS
 TITLE REPORT BY THE DEPT. OF TRADE ON THE ACTION TAKEN TO DEAL WITH THE OIL SPILLED AS A RESULT OF THE COLLISION IN THE OYSTER STRAIT ON NOV. 12, 1975 BETWEEN THE 1971 OLYMPIC ALLIANCE AND HMS ACHILLES ESSO EUROPE INC. LIBRARY, 1976
 ABST THIS REPORT REFERS TO THE LAND BASED OPERATION, BUT IS PRIMARILY CONCERNED WITH THE COUNTRY MEASURES TAKEN AT SEA. THERE IS AN ANNEX WHICH DESCRIBES THE ANTI-OIL POLLUTION ORGANIZATION NATIONALLY AND THE FACILITIES AVAILABLE TO IT, DISPERSANTS, ORGANIZATIONS, COUNTERMEASURES AT SEA
 KEY CODE 7081F

AUTH ANONYMOUS
 TITLE REPORT OF ACTIVITIES
 PUBL 3RD SEA OIL SERVICES SPA, AUG. 1969
 ABST A DESCRIPTION OF VARIOUS PROJECTS UNDERTAKEN BY SSO'S, THEIR PROCEDURES AND RESULTS. INCLUDES MANY PHOTOGRAPHS OF EQUIPMENT AND EXPLANATIONS OF THEM.
 CODE 3040R

AUTH ANONYMOUS
 TITLE REPORT OF THE NATIONAL PLANNING CONFERENCE ON THE COMMERCIAL DEVELOPMENT OF THE OCEANS VOL. II PROGRAM ELEMENTS
 PUBL ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION, US DEPT. OF COMMERCE, JUNE 1970, PB 265 705, OCE 5-30024
 ABST VOL. II CONTAINS ALL OF THE PROGRAM ELEMENTS THAT WERE RECOMMENDED BY THE CONFERENCE.
 REYN OCEAN BASINS, ENVIRONMENTS, MARINE TRANSPORT
 CODE 7212AF

AUTH ANONYMOUS
 TITLE REPORT OF THE NATIONAL PLANNING CONFERENCE ON THE COMMERCIAL DEVELOPMENT OF THE OCEANS VOL. I. CONFERENCE ADDRESSES AND SUMMARY
 PUBL NOAA, ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION, PB 265 704, OCE 5-30024, JUNE 19-22, 1970
 ABST CONFERENCE HELD IN WASHINGTON, D.C. AND ARLIE, VA., JUNE 1970. VOL. I CONTAINS THE ADDRESSES THAT OPENED THE SESSION AND THE SYNOPSIS REPORTS PRESENTED AT THE END OF THE SESSION.
 REYN OCEAN BASINS, ENVIRONMENTS, MARINE TRANSPORT
 CODE 7212F

AUTH ANONYMOUS
 TITLE A REPORT ON POLLUTION OF THE NATION'S WATERS BY OIL AND OTHER HAZARDOUS SUBSTANCES
 PUBL SECY OF INTERIOR, SECY OF TRANSPORTATION, FEB. 1968
 ABST A STUDY TO EXAMINE HOW THE RESOURCES OF THE US COULD BEST BE MOBILIZED AGAINST THE POLLUTION OF WATER BY SPILLS OF OIL AND OTHER HAZARDOUS SUBSTANCES.
 CODE 6018R

AUTH ANONYMOUS
 TITLE REPORT ON THE NORTH SEA OIL SPILL
 PUBL U.S. ENVIRONMENTAL SCIENTISTS TEAM, U.S. DEPT. OF THE INTERIOR, FISH AND WILDLIFE SERVICE, MAY 1972
 ABST THIS PAPER IS A TEAM REPORT ON THE NORTH SEA OIL SPILL.
 REYN RESPONSE, OIL SPILL, NORTH SEA
 CODE 1232F

AUTH ANONYMOUS
 TITLE REPORT TO THE PRESIDENT AND CONGRESS
 PUBL SECRETARY OF TRANSPORTATION, 92ND CONGRESS, APRIL 1971
 ABST OIL POLLUTION LIABILITY AND FINANCIAL RESPONSIBILITY
 CODE 6053R

AUTH ANONYMOUS
 TITLE RESEARCH AND DEVELOPMENT AND MONITORING PROGRAMS TO ASSESS OIL SPILL EFFECTS
 PUBL OCEAN SCIENCE NEWS, JULY 4, 1972
 ABST THIS MATERIAL POINTS OUT THE NEED FOR A UNCLE SAM SYSTEM CONCEPT IN THE AREA OF RESEARCH, DEVELOPMENT AND MONITORING PROGRAMS TO ASSESS OIL SPILL EFFECTS ON THE MARINE ENVIRONMENT.
 REYN GOVERNMENT AGENCIES, DAMAGE ASSESSMENT, RESEARCH
 CODE 2660F

AUTH ANONYMOUS
 TITLE RESEARCH AND DEVELOPMENT FOR A SHIPBOARD OIL AND WATER SEPARATION SYSTEM
 PUBL US DEPT. OF COMMERCE, PROJECT NO. D1080334, JUNE 1963
 ABST A REANS OF SEPARATION WAS DEVELOPED WHICH INVOLVED THE USE OF A CAPACITANCE PROBE TO DIVERT THE RELATIVELY SMALL AMOUNT OF BALLAST WATER CONTAINING OVER ONE PERCENT OIL TO A HOLDING TANK OF EXISTING BALLAST TANK. THE REMAINDER OF THE WATER, WITH LESS THAN ONE PERCENT THROUGH A SERIES OF DUTCH WAVE CUMESKING SCREENS.
 REYN SEPARATION, CAPACITANCE PROBE BALLAST WATER
 CODE 0062R

AUTH ANONYMOUS
 TITLE RESEARCH AND DEVELOPMENT FOR A SHIPBOARD OIL AND WATER SEPARATION SYSTEM
 PUBL US DEPT. OF COMMERCE, MARITIME ADMINISTRATION, CONTRACT NO. MA-2721, DEC. 1966
 ABST PART I OF THIS INVESTIGATION WAS TO OBTAIN INFORMATION ON WHICH TO BASE THE DEVELOPMENT OF A

- PRACTICAL PACKAGE TYPE UNIT SUITABLE FOR SHIPBOARD
 SEPARATION OF BALLAST WATER FROM NUMBER C FUEL
 OIL. PART II DESCRIBES A LONG BASIC PROTOTYPE UNIT
 CONSTRUCTED AND TESTED AT POINT ROBBIL, STATES
 ISLAND, NY.
 REVD SEPARATION, SHIPBOARD USE, BALLAST WATER,
 PROTOTYPE, COMESENCE, FILTRATION BARRIERS
 CODE 5125F
- AUTH ANONYMOUS
 TITLE RESEARCH AND DEVELOPMENT PLANS, VOL. 2,
 (RESTRICTED)
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
 NO. T1402/002-2
 CODE 8749A
- AUTH ANONYMOUS
 TITLE RESEARCH DEVELOPMENT AND DEMONSTRATION PROJECTS ON
 OIL POLLUTION CONTROL
 PUBL OIL AND HAZARDOUS MATERIALS RESEARCH SECTION,
 EDISON WATER QUALITY LABORATORY, SEPT. 1970
 ABST INDEX - LISTS PROJECTS ON OIL POLLUTION CONTROL
 CODE 8040A
- AUTH ANONYMOUS
 TITLE RESEARCH NEEDED TO DETERMINE CHRONIC EFFECTS OF
 OIL ON THE MARINE ENVIRONMENT
 PUBL EXXON COMPANY, NOV. 4-8, 1974
 ABST DELIBERATIONS AND RECOMMENDATIONS OF A WORKSHOP.
 REVD IDENTIFICATION, MEASUREMENT, MARINE ENVIRONMENT,
 FUNDING
 CODE 3513F
- AUTH ANONYMOUS
 TITLE RESEARCH NEEDED TO DETERMINE EFFECTIVENESS OF
 CHEMICALS IN TREATING OIL SPILLS AND THE TOXICITY
 OF CHEMICALLY DISPERSED OIL
 PUBL EXXON PRODUCTION RESEARCH CO.
 ABST DELIBERATIONS AND RECOMMENDATIONS OF A WORKSHOP
 SPONSORED BY EXXON PRODUCTION RESEARCH COMPANY,
 HELD IN HOUSTON, TEXAS, NOVEMBER 29-30, 1974. A
 PANEL OF 14 RECOGNIZED INTERNATIONAL SCIENTISTS
 MET AND CONSIDERED RESEARCH NEEDED TO DETERMINE THE
 EFFECTIVENESS OF CHEMICALS TO ACCELERATE
 NATURAL PROCESSES IN THE ENVIRONMENT, PRIMARILY
 DISPERSION, ACTING ON OIL SPILLS; (2) THE
 EFFECTS ON THE MARINE ENVIRONMENT (TOXICITY) BOTH
 ACUTE AND CHRONIC OF OIL SPILLS TREATED WITH
 CHEMICALS COMPARED WITH UNTREATED SPILLS.
 REVD OIL SPILL, CHEMICAL, DISPERSANT
 CODE 7749F
- AUTH ANONYMOUS
 TITLE RESPONSES TO: "CRISIS SCIENCE: INVESTIGATIONS IN
 RESPONSE TO THE AGG. MERCHANT OIL SPILL" BY
 STOLZENBACH AND PARSONS
 PUBL M.S.I. GRADUATE SCHOOL OF OCEANOGRAPHY, DEC. 1977
 ABST COMMENTS ON THE ABOVE ARTICLE FROM VARIOUS UNIT
 FACULTY MEMBERS.
 REVD OIL SPILL, AGG. MERCHANT
 CODE 7054F
- AUTH ANONYMOUS
 TITLE RESULTS OF OVERSIGHT OF CHEVRON OIL SPILL IN THE
 GULF OF MEXICO
 PUBL NASA, AD 714 681
 CODE 0213A
- AUTH ANONYMOUS
 TITLE RESULTS OF THE REGION I WORKSHOP ON OIL SPILL
 ECOLOGICAL DAMAGE ASSESSMENT
 PUBL RETRAIR DIVISION THE RETRAIR CORPORATION
 ABST THE MAJOR AIM OF THE WORKSHOP WAS TO IDENTIFY
 SCIENTIFIC NEEDS AND RESOURCES THAT MIGHT BE
 INCORPORATED IN A NEW ENGLAND REGIONAL RESPONSE
 PLAN FOR ECOLOGICAL DAMAGE ASSESSMENT
 REVD ASSESSMENT, DISPERSANTS, OIL SPILL
 CODE 7726F
- AUTH ANONYMOUS
 TITLE A REVIEW OF MECHANICAL SYSTEMS FOR THE RECOVERY OF
 OIL SPILLED ON WATER
 PUBL INSTITUTE OF PETROLEUM, CANAD. CON. FOR THE PREV.
 OF SEA POLL. APRIL 1974
 CODE 0125A
- AUTH ANONYMOUS
 TITLE A REVIEW OF THE DRAFT ENVIRONMENTAL IMPACT
 STATEMENT ON THE PROPOSED WATER CONTINENTAL SHELF
 OIL AND GAS LEASE SALE (NO. 42) OFFSHORE THE NORTH
 ATLANTIC STATES
 PUBL COASTAL RESOURCES CENTER, M.S.I. GRADUATE SCHOOL OF
 OCEANOGRAPHY, NOV. 3, 1970
 ABST THIS REPORT IS TO PERFORM A REVIEW OF ALL SECTIONS
 WITH EMPHASIS ON TECHNICAL CONTENT AND QUALITY
 REVD ENVIRONMENTAL IMPACT, LEASES, TECHNICAL CONTENT
 CODE 0185B
- AUTH ANONYMOUS
 TITLE REVIEW OF THE SANTA BARBARA CHANNEL OIL POLLUTION
 INCIDENT
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT
 NO. T1402/003
 CODE 0750A
- AUTH ANONYMOUS
- TITLE BFO/SAMP/DIC BOUW
 PUBL REPORT NO. INT 86, HYDRAULICS RESEARCH STATION,
 1971
 CODE 0735A
- AUTH ANONYMOUS
 TITLE SAN FRANCISCO OIL SPILL
 PUBL SPECIAL SUBCOMMITTEE, 92ND CONGRESS, FEB. 8-9,
 1971
 ABST HEARINGS ON TANKER COLLISION OF JAN. 8, 1971 IN
 SAN FRANCISCO BAY BETWEEN ARIZONA STANDARD AND
 OREGON STANDARD AND EFFECTS OF RESULTING MASSIVE
 OIL SPILL.
 REVD OIL SPILL, SAN FRANCISCO
 CODE 6031R
- AUTH ANONYMOUS
 TITLE SANTA BARBARA - OIL POLLUTION, BIOLOGICAL EFFECTS
 PUBL UNIV. OF CALIF., OCT. 1970
 ABST 1969 STUDY OF BIOLOGICAL EFFECTS OF OIL SPILL
 WHICH OCCURRED AT SANTA BARBARA CAL. IN 1969.
 CODE 6021R
- AUTH ANONYMOUS
 TITLE SANTA BARBARA OIL SPILL: SHORT-TERM ANALYSIS OF
 MACROPLANKTON AND FISH
 PUBL SPA, CONTRACT NO. 14-12-534, PROJECT NO. 15000CAL,
 1971
 ABST COLLECTIONS OF DEEP AND SHALLOW MACROPLANKTON FROM
 THE SANTA BARBARA CHANNEL AREA OF THE 1969 OIL
 SPILL AND FROM THE SANTA BARBARA BASIN FURTHER
 OFFSHORE WERE COMPARED WITH OTHERS FROM PREVIOUS
 YEARS FOR POSSIBLE OIL DAMAGE.
 REVD MACROPLANKTON, SANTA BARBARA CHANNEL, ANALYSIS
 CODE 0550A
- AUTH ANONYMOUS
 TITLE SANTA BARBARA OIL SYMPOSIUM
 PUBL UNIVERSITY OF CALIFORNIA AT SANTA BARBARA,
 OFFSHORE PETROLEUM PRODUCTION: AN ENVIRONMENTAL
 INQUIRY, DEC. 10-14, 1970
 ABST THE PURPOSE OF THE SYMPOSIUM WAS TO ASSEMBLE A
 GROUP OF KNOWLEDGEABLE SPEAKERS TO DISCUSS THE
 EFFECTS OF THE SANTA BARBARA OIL SPILL OF JAN. 24,
 1969.
 REVD OIL SPILL, SYMPOSIUM
 CODE 4003B
- AUTH ANONYMOUS
 TITLE SEA GUARDIAN
 PUBL GEMMA PLASTICS FABRICATORS INC.
 ABST THESE BULLETINS DESCRIBE SEVERAL OIL SPILL
 CONTAINMENT BOOMS AND ACCESSORIES.
 CODE 3069F
- AUTH ANONYMOUS
 TITLE SEADUP MOPS OIL SPILLS
 PUBL MECHANICAL ENGINEERING MAY 1974
 CODE 0380A
- AUTH ANONYMOUS
 TITLE SEARCH MOUNTS FOR SIX MEN MISSING AFTER SHIP HITS
 OIL RIG
 PUBL PROVIDENCE JOURNAL BULLETIN, AUG. 20, 1975
 ABST A BRITISH TANKER, THE GLOBIA SAN, SANKED INTO AN
 OFFSHORE DRILLING PLATFORM.
 REVD TANKER, ACCIDENTS, OFFSHORE DRILLING PLATFORM
 CODE 7043F
- AUTH ANONYMOUS
 TITLE SEPARATORS
 PUBL OILLEKENICAL SEPARATOR CO.
 ABST THIS BULLETIN DESCRIBES SEVERAL SEPARATORS USED
 FOR SEPARATION OF EMULSIFIED OILS FROM WATER.
 CODE 3060F
- AUTH ANONYMOUS
 TITLE SHIP GENERATED POLLUTION TANKER AND NON TANKER
 UNKNOWN
 ABST THIS PAPER PRESENTS ESTIMATES AND PROJECTIONS OF
 TANKER DISCHARGE AND LEGISLATURE REGARDING
 DISCHARGES.
 REVD TANKERS, DISCHARGES, LEGISLATION
 CODE 5009F
- AUTH ANONYMOUS
 TITLE SEAMER FLOATS OIL OUT OF WATER
 PUBL MACHINE DESIGN, 1974
 CODE 0370A
- AUTH ANONYMOUS
 TITLE SEAMER PUMPING RATE ADJUSTABLE TO 300 GPM
 PUBL OIL AND GAS JOURNAL, 1974
 CODE 0373B
- AUTH ANONYMOUS
 TITLE SLICK SOLUTION
 PUBL SURFACE SEPARATOR SYSTEMS, AUG. 1962
 ABST OIL SLICKS FROM SPILLAGE AROUND TANKER BERTHS
 COMBINED BY FLOATING BARRIER OF NEOPRENE COATED
 FABRIC PLYWOODS.
 CODE 6015A
- AUTH ANONYMOUS
 TITLE SLICK TRIMMING
 PUBL THE UNIVERSITY OF MICHIGAN, COLLEGE OF

- ENGINEERING, JULY 1975
 ABST A REPORT ON CONTAINMENT DEVICES TESTED, CLEANUP, HYDROPHOBIC HOP, OLEOPHILIC HOP, CONTAINMENT DEVICES, PICKUP DEVICES, BARRIERS, HEADERS
 REYN HEADERS
 CODE 29774
- AUTH ANONYMOUS
 TITLE SOLUBILITY IN WATER OF NORMAL C9 AND C10 HYDROCARBONS
 PUBL SCIENCE
 ABST A NEW METHOD FOR EQUILIBRATING WATER CONTAINING ALKANE HYDROCARBONS WITH GAS PHASE AND ANALYZING THE GAS PHASE CHROMATOGRAPHY SETTING ANALYTICAL SENSITIVITY TO BETTER THAN 0.1 PART PER BILLION.
 CODE 26314
- AUTH ANONYMOUS
 TITLE SOURCE EFFECTS AND SINKS OF HYDROCARBONS IN THE AQUATIC ENVIRONMENT
 PUBL AMERICAN INSTITUTE OF BIOLOGICAL SCIENCES AUGUST 9-11 1976
 ABST PROCEEDINGS OF THE SYMPOSIUM AMERICAN UNIVERSITY WASHINGTON DC AUGUST 9-11 1976. A SUMMARY LOOK AT THE EFFECTS OF CURRENT PRACTICES & PROCEDURES UPON BIOLOGICAL SYSTEMS INVOLVING THE INDUSTRIAL, GOVERNMENTAL, AND ACADEMIC AND WORKERS. CONSIDERING THE LOW RANGE AS WELL AS THE SHORT RANGE EFFECTS.
 REYN HYDROCARBONS, WASTE DISPOSAL RECOVERY, TRANSPORT
 CODE 4040 B
- AUTH ANONYMOUS
 TITLE SPECIFICATION FOR MECH. OIL BARRIER SYSTEMS
 PUBL MIL. ENG. REP-7-235, USCG, OCEAN ENGR. DIV., NOV. 1971
 CODE 07194
- AUTH ANONYMOUS
 TITLE SPECIFICATION FOR MECHANICAL OIL BARRIER SYSTEM CLEANING/ENGINEERING DIVISION, US COAST GUARD, REPLACED NO. ECE-2-235, NOV. 26, 1971
 ABST DESCRIBES SPECIFICATION OF A COMMERCIAL TYPE MECHANICAL FLOATING OIL BOOM.
 REYN CONTAINMENT, CONTROL, BOOMS
 CODE 08737
- AUTH ANONYMOUS
 TITLE SPILL TRAINING AND EDUCATIONAL PROGRAM
 PUBL TEXAS A & M, CONTRACT NO. E 14621 4965 WITH USERA
 ABST INCLUDES HISTORY AND EARLY HISTORIES OF OIL SPILLS, NATIONAL POLICY, PROPERTIES OF OIL, CONTAINMENT, REMOVAL, DISPOSAL, SPILLS IN THE ENVIRONMENT, RECURRENT PROCEDURES FOR USE OF OIL SPILL BATTALIONS, LEGAL, COSTS OF CLEANUP, CONTINGENCY PLANNING, AND OIL SPILLS, OPERATION RESCUE, SUGGESTED PRIORITIES FOR DEVELOPMENT OF SPILL PREVENTION CONTROL AND CONTINGENCY PLANS.
 REYN REMOVAL, CONTAINMENT, DISPOSAL, CONTINGENCY, CLEANUP, PREVENTION
 CODE 76646
- AUTH ANONYMOUS
 TITLE STANDARD DISPERSANT EFFECTIVENESS AND TOXICITY TEST
 PUBL NATIONAL ENVIRONMENTAL RESEARCH CENTER, OFFICE OF RESEARCH AND MONITORING, EPA R2-73-261, MAY 1973
 ABST A BRIEF HISTORY OF THE DEVELOPMENT OF THE STANDARD EPA DISPERSANT EFFECTIVENESS IS DISCUSSED.
 REYN DISPERSANTS, TOXICITY
 CODE 25304
- AUTH ANONYMOUS
 TITLE STORAGE WASTES FROM WATER CRAFT AND DISPOSAL AT SHORE FACILITIES
 PUBL EPA, CONTRACT NO. 14-12-509
 ABST TO TEST THE EFFECTIVENESS AND ACCEPTABILITY OF A WATERCRAFT EMPLOYMENT SYSTEM IN CONTROLLING WASTE SOURCES, SANITARY AND GALLEY WASTE, DEMONSTRATION UNIT WAS DESIGNED AND BUILT AND TEST DATA WAS ANALYZED AND EVALUATED.
 REYN WATERCRAFT EMPLOYMENT SYSTEM, CONTROLLING WASTE SURFACES
 CODE 00494
- AUTH ANONYMOUS
 TITLE STUDIES OF OIL RETENTION BOOM HYDRODYNAMICS
 PUBL HYDRODYNAMICS INC. 40 719 294
 CODE 01734
- AUTH ANONYMOUS
 TITLE STUDY OF HYDRAULIC MEMBRANES FOR OIL-WATER SEPARATION
 PUBL USCG
 ABST HYDRAULIC MEMBRANES, OIL-WATER SEPARATION
 CODE 02484
- AUTH ANONYMOUS
 TITLE A STUDY OF SPRAY ON LINES FOR PETROLEUM PRODUCT STORAGE AREAS ON THE NORTH
 PUBL EBA ENGINEERING CONSULTANTS, EPS REPORT NO. EPS-4-EC-77-2, FEB. 1977
 ABST THIS PAPER DISCUSSES A SPRAY ON LINES SYSTEM FOR STORAGE AREAS IN THE NORTH
 REYN SPRAY ON LINES SYSTEM, STORAGE AREAS, RETENTION
 CODE 71004
- AUTH ANONYMOUS
 TITLE A STUDY OF THE BEHAVIOR OF OIL SPILLS IN THE ARCTIC
 PUBL USCG, AD 717 142
 REYN ARCTIC, BEHAVIOR, STUDY
 CODE 01954
- AUTH ANONYMOUS
 TITLE SUMMARY OF Awarcs 1975 DIVISION OF ADVANCED ENVIRONMENTAL RESEARCH AND TECHNOLOGY
 PUBL NATIONAL SCIENCE FOUNDATION
 ABST THIS REPORT PRESENTS BRIEF SUMMARIES OF PROJECTS FUNDED BY THE DIVISION OF ADVANCED ENVIRONMENTAL RESEARCH AND TECHNOLOGY IN 1975, AND PROJECTS FUNDED DURING PREVIOUS YEARS THAT WERE ACTIVE DURING THAT PERIOD. REPORT DESCRIBES THE NATURE OF THE DIVISION'S SEVEN PROGRAMS: ENVIRONMENTAL EFFECTS OF ENERGY, TRACE CONTAMINANTS; REGIONAL ENVIRONMENTAL MANAGEMENT; EARTHQUAKE ENGINEERING; FIRE RESEARCH; SOCIOECONOMIC RESPONSE TO NATURAL HAZARDS; WEATHER MODIFICATION
 REYN ENVIRONMENTAL IMPACTS, POLLUTION, HAZARDS, FIRES
 CODE 2674 F
- AUTH ANONYMOUS
 TITLE SUMMARY OF CAPABILITIES
 PUBL US ARMY CORPS. OF ENGINEERS, COASTAL ENGINEERING RESEARCH CENTER, PAPER NO. 3-04
 ABST THE MISSION, HISTORY, ORGANIZATION, AND PHYSICAL FACILITIES OF THE COASTAL ENGINEERING CENTER ARE PRESENTED.
 CODE 30414
- AUTH ANONYMOUS
 TITLE SUMMARY OF COSTS OF COMBATING OIL SPILLS
 PUBL DEPT. OF MECHANICAL ENGINEERING AND APPLIED MECHANICS, JAN. 1970
 ABST COMBATING SPILLS, COST EVALUATION, CLEANUP
 CODE 50904
- AUTH ANONYMOUS
 TITLE SUMMARY OF MIT HYDRODYNAMICS STUDIES
 PUBL 454 ENVIRONMENTAL TECHNOLOGY GROUP-CLEAN TECHNOLOGY DIVISION, NAVAL UNDERWATER SYSTEMS CENTER, NEWPORT, RI, FEB. 1978
 ABST THE OVERALL OBJECTIVE OF THIS PROGRAM IS TO DETERMINE THE INFLUENCE OF OIL SLICER CHEMICAL COMPOSITION AND PHYSICAL PROPERTIES ON OIL SLICER DISPERSION.
 REYN TURBULENCE, WIND/WAVE, DISPERSION
 CODE 26604
- AUTH ANONYMOUS
 TITLE SUPPORT SYSTEMS TO DELIVER AND MAINTAIN OIL RECOVERY SYSTEM AND DISPOSAL OF RECOVERED OIL
 PUBL BATTALIE COLUMBIEN, JAN. 1976, AD 778 941
 CODE 01874
- AUTH ANONYMOUS
 TITLE SUMMARY COLLECTING AGENTS
 PUBL SMELL OIL SL. LOSS PREVENTION DEPT., MARCH 1972
 ABST VARIOUS ARTICLES
 REYN COLLECTING AGENTS, SPREADING, OIL HEADER
 CODE 76764
- AUTH ANONYMOUS
 TITLE SURFACE SKIMMER FOR RECOVERING PULL OIL SPILLS FROM WATER SURFACE
 PUBL FLORECA POWLA AND LIGHT CO., SSEE NO. AO-676
 CODE 06474
- AUTH ANONYMOUS
 TITLE SURVEY OF COMMERCIAL OIL-WATER SEPARATIONS
 PUBL USCG, 6-D17-1, AUG. 1973
 CODE 02314
- AUTH ANONYMOUS
 TITLE SURVEY STUDY TO SELECT A LIMITED NUMBER OF HAZARDOUS MATERIALS TO DEFINE ANALYTICAL REQUIREMENTS, VOL. 1
 PUBL USCG, MARCH 1974
 CODE 02584
- AUTH ANONYMOUS
 TITLE SURVEYS AND INVESTIGATIONS TO DETERMINE SOURCES, CAUSES, EFFECTS AND MOVEMENT IN DISPERSION OF OIL AND HAZARDOUS SUBSTANCES SPILLED IN THE COASTAL AND ESTUARINE ZONES
 PUBL RFP WA 72-3, EPA, OCT. 18, 1971
 CODE 20594
- AUTH ANONYMOUS
 TITLE TANKER OIL SPILLS
 PUBL WESTERN CO. OF NORTH AMERICA, RESEARCH DIVISION, JAN. 1971
 ABST GETTING LAUDE OILS TO REDUCE MARINE POLLUTION FROM TANKER OIL SPILLS.
 CODE 60494
- AUTH ANONYMOUS
 TITLE TECHNICAL DATA BOOK - PETROLEUM REFINING
 PUBL API
 ABST CHAPTERS 7-14, TECHNICAL DATA BOOK OF OIL REFINING
 REYN TECHNICAL DATA, REFINING
 CODE 61774

- AUTH ANONYMOUS
 TITL TECHNICAL PROGRESS REPORT - YEAR ONE, 1975-1976, A FACILITY FOR THE EXPERIMENTAL ANALYSIS OF COASTAL MARINE ECOSYSTEMS
 PUBL URI, GRADUATE SCHOOL OF OCEANOGRAPHY
 ABST THE PROGRESS REPORT COVERS PERFORMANCE DURING THE FIRST THREE QUARTERS OF THE YEAR WITH ACTIVITIES PROJECTED FOR THE FOURTH QUARTER. REPLICATE Meso-SCALE EXPERIMENTAL ECOSYSTEMS SIMULATING A VARIETY OF COMMON COASTAL MARINE ENVIRONMENTS WILL BE DEVELOPED AND MAINTAINED AT A SPECIAL SAGRE BASED LAB.
 RESEARCH, DEVELOPMENT, INDOU.
 KEYW Meso-SCALE, ECOSYSTEMS, COASTAL MARINE ENVIRONMENT
 CODE 7683F
- AUTH ANONYMOUS
 TITL A TECHNIQUE FOR PREDICTING THE MOVEMENT OF OIL SPILLS IN NEW YORK HARBOR
 PUBL FEB. 1974, AD 786 627
 CODE 0229R
- AUTH ANONYMOUS
 TITL A TECHNIQUE FOR PREDICTING THE MOVEMENT OF OIL SPILLS IN NEW YORK HARBOR
 PUBL USCG, NATIONAL TECHNICAL INFORMATION SERVICE, AD 786627, FEB. 1975
 ABST A SIMPLE METHOD OF FORECASTING THE MOVEMENT OF AN OIL SLICK WITHIN THE HARBOR.
 KEYW FORECASTING, MOVEMENT, HARBORS
 CODE 3012R
- AUTH ANONYMOUS
 TITL TENTATIVE METHODS FOR COMPARISON OF WATERBORNE PETROLEUM OILS BY GAS CHROMATOGRAPHY
 PUBL ASTM, DESIG., D3320-74A1
 ABST THIS PAPER DISCUSSES THE METHODS OF COMPARISON OF PETROLEUM OILS RECOVERED FROM WATER OFF BEACHES.
 KEYW RECOVERY, GAS CHROMATOGRAPHY, SAMPLE ANALYSIS
 CODE 1229F
- AUTH ANONYMOUS
 TITL TENTATIVE PRACTICE FOR IDENTIFICATION OF WATERBORNE OILS
 PUBL ASTM, D-3415-75I
 ABST THIS PAPER DISCUSSES THE BROAD CONCEPTS OF SAMPLING AND ANALYZING WATERBORNE OILS FOR IDENTIFICATION AND COMPARISON WITH SOURCE OILS.
 KEYW IDENTIFICATION, CHEMICAL CHARACTERIZATION, SAMPLING AND ANALYZING
 CODE 1228F
- AUTH ANONYMOUS
 TITL TESTING AND EVALUATION OF OIL SPILL RECOVERY EQUIPMENT
 PUBL EPA, WATER QUALITY OFFICE, REPT. NO. PB 200 001
 ABST A DETAILED REPORT CONTAINING BOTH THE TEST RESULTS ON THE CAPABILITIES AND LIMITATIONS OF THE VARIOUS EQUIPMENT TYPES WERE TESTED.
 KEYW RECOVERY, CURTAIN BOOMS, FENCE BOOMS, AIR BARRIERS, SWIMMERS
 CODE 0408F
- AUTH ANONYMOUS
 TITL TESTING AND EVALUATION OF OIL SPILL RECOVERY EQUIPMENT
 PUBL WATER POLLUTION CONTROL SERIES EPA, REPORT NO. 1504002 1270
 KEYW BARRIERS, SWIMMERS
 CODE 0715R
- AUTH ANONYMOUS
 TITL THEORETICAL STUDY TO DETERMINE THE SLA STATE LIMIT FOR THE SURVIVAL OF OIL SLICKS ON THE OCEAN
 PUBL ARTHUR D. LITTLE, INC. AD. NO. 70244, FEB. 1977
 ABST THE RESULTS FROM THIS PROGRAM ARE DISCUSSED UNDER TWO BRAD CLASSIFICATIONS. THOSE OBTAINED FROM THE BACKGROUND STUDY-LITERATURE SEARCH AND THOSE RESULTING FROM THE PHYSICAL MODELS DEVELOPED.
 KEYW TRANSPORT, TANKERS, OIL DISCHARGE
 CODE 0130D
- AUTH ANONYMOUS
 TITL TIDAL CURRENT TABLES 1979, ATLANTIC COAST OF NORTH AMERICA
 PUBL NOAA NATIONAL OCEAN SURVEY
 ABST DAILY PREDICTED TIMES OF SLOW WATER AND PRELICTED TIMES & VELOCITIES OF MAXIMUM CURRENT (FLOW AND EBB) ARE PRESENTED IN A TABLE FOR A NUMBER OF REFERENCE STATIONS. CURRENT DIAGRAMS ARE GIVEN FOR A NUMBER OF IMPORTANT CHANNELS AND AN INDEX OF THE STATIONS IS ALSO GIVEN.
 KEYW TIDAL CURRENTS, OCEAN TIDES, OCEANOGRAPHIC DATA
 CODE 7701 F
- AUTH ANONYMOUS
 TITL THE TROPOSPHERIC TRANSPORT OF POLLUTANTS AND OTHER SUBSTANCES TO THE OCEANS
 PUBL NATIONAL ACADEMY OF SCIENCES
 ABST WORKSHOP WAS HELD ON DECEMBER 8-12, 1975. THE ULTIMATE OBJECTIVE OF EACH PANEL WAS TO PRODUCE A REPORT THAT CRITICALLY SUMMARIZED PRESENT KNOWLEDGE AND MADE SPECIFIC AND REALISTIC RECOMMENDATIONS AS TO THE TYPES OF MEASUREMENTS AND PROGRAMS THAT WOULD BE NECESSARY IN ORDER TO MAKE AN ACCURATE ASSESSMENT OF ATMOSPHERIC TRANSPORT FLUXES TO THE OCEANS.
- KEYW MODELING, HYDROCARBONS, RADIONUCLIDES, TROPOSPHERIC
 CODE 7716 F
- AUTH ANONYMOUS
 TITL U.S./N.A.C.D.
 PUBL GOVERNMENT DATA PUBLICATIONS, SEPT. 1976
 ABST A RESEARCH AND DEVELOPMENT INDOU.
 KEYW RESEARCH, DEVELOPMENT, INDOU
 CODE 7605F
- AUTH ANONYMOUS
 TITL ULTRASONIC EMULSIFICATION OF OIL TANKER CARGO SONICS INTERNATIONAL INC., FEDERAL WATER POLLUTION CONTROL ADMINISTRATION, DEPT. OF THE INTERIOR, APRIL 1976, NO. PB 192 633
 ABST THE ULTRASONIC EMULSIFICATION OF OIL FOR MARINE TRANSPORTATION HAS BEEN TESTED FOR FEASIBILITY, AS A POLLUTION PREVENTATIVE CONCEPT.
 KEYW CONTINUOUS PROCESS, TOXICITY, TANKER, ULTRASONICS, EMULSION STABILITY
 CODE 5038F
- AUTH ANONYMOUS
 TITL US CHECKING UP ON FIRMS SPILL PREVENTION PLANS
 PUBL OIL AND GAS JOURNAL, VOL. 72, NO. 30, JULY 29, 1974
 ABST SPOI CHECKS ON INDUSTRIES AND ENCOURAGEMENT TO CONTAIN OIL SPILLS.
 CODE 3121R
- AUTH ANONYMOUS
 TITL US VS. BOTE
 PUBL POLLUTION CONTROL GUIDE, VOL. 3, 6-3-74
 ABST DISCHARGE OF OIL INTO NAVIGABLE WATERS, DEPENDENT COMPLIANCE LAWS WERE VAGUE, COLAT UNHELD LAWS.
 CODE 3131R
- AUTH ANONYMOUS
 TITL USE OF CHEMICALS TO TREAT OIL ON WATER - STATUS REPORT
 PUBL NORTHWEST REGION RESEARCH AND DEVELOPMENT PROGRAM, REPORT NO. PB 215 044, FEB. 20, 1969
 ABST THIS PAPER DISCUSSES FACTORS TO BEAN IN MIND WHEN USING CHEMICALS TO TREAT OIL IN WATER.
 KEYW DISPERSANTS, ENVIRONMENT, FLOATING ABSORBENTS, SINKING AGENTS, GELLING AGENTS, BURNING AGENTS
 CODE 2919F
- AUTH ANONYMOUS
 TITL USE OF DISPERSANTS FOR OIL POLLUTION SUBMITTED BY THE UNITED KINGDOM
 PUBL MARINE ENVIRONMENT PROTECTION COMMITTEE, 1974/1979, JUNE 30, 1975
 ABST LIST OF DISPERSANTS WHICH HAVE BEEN AUTHORIZED FOR USE AT SEA, IN COASTAL WATERS AND BEACHES AROUND THE UNITED KINGDOM.
 KEYW DISPERSANTS, UNITED KINGDOM
 CODE 5077F
- AUTH ANONYMOUS
 TITL THE USE OF LARGE MARINE MICROCOSMS TO STUDY THE PATES AND EFFECTS OF CHRONIC LOW LEVEL POLLUTANTS
 PUBL THE MARINE ECOSYSTEMS RESEARCH LABORATORY, GRADUATE SCHOOL OF OCEANOGRAPHY, URI, 1976
 ABST CONTROLLED EXPERIMENTS IN MICROCOSMS OF THE NATURAL ECOSYSTEM PROVIDE AN OPPORTUNITY TO ACQUIRE DETAILED QUANTITATIVE UNDERSTANDING OF THE VARIOUS TYPES OF PROCESSES AFFECTING THE TRANSFER AND DEGRADATION OF SUBSTANCES IN NATURE AND ON THE EFFECTS SUCH SUBSTANCES MIGHT HAVE ON COASTAL MARINE ECOSYSTEMS. ACCORDINGLY, LARGE MICROCOSMS WERE ESTABLISHED AT THE MARINE ECOSYSTEM RESEARCH LABORATORY (MERL) TO PROVIDE SUCH INFORMATION TO THE EPA.
 KEYW MICROCOSMS, ECOSYSTEMS, BIOLOGICAL & CHEMICAL
 CODE 7730F
- AUTH ANONYMOUS
 TITL USING CHEMICALS FOR CLEANING UP OIL SPILLS
 PUBL OCEAN INDUSTRY, VOL. 5, NO. 8, AUG. 1970,
 POLLUTION CONTROL REPORT, PART 3
 ABST THIS PAPER DISCUSSES METHODS FOR CLEANING UP.
 KEYW CLEANUP, DISPERSANTS
 CODE 3126F
- AUTH ANONYMOUS
 TITL VIADNA SYSTEM DESIGNED TO CONTROL AND LIMIT OIL SPILLS OCCURRING AT SEA
 PUBL OIL AND GAS JOURNAL
 CODE 0309R
- AUTH ANONYMOUS
 TITL VORTEX CONCEPT FOR SEPARATING OIL FROM WATER
 PUBL UNITED AIRCRAFT RESEARCH LABS., JAN. 1973, AD 758 320
 CODE 0232R
- AUTH ANONYMOUS
 TITL VORTEX SEPARATION FOR OIL SPILL RECOVERY SYSTEMS
 PUBL AMERICAN PROCESS EQUIPMENT CORP.
 ABST TWO PHASE PROGRAM, DESIGN, FABRICATE, AND TEST A 1000 PROTOTYPE OIL/WATER SEPARATOR, PHASE 1: EXPERIMENTAL 50 GPM SEPARATOR BUILT AND TESTED. PHASE 2: FULL SCALE PROTOTYPE TESTED BY STANDARD OIL CO. NOTE: PUBLISHED FOR THE WATER QUALITY OFFICE, EPA.

REYN WASTE SEPARATION, RECOVERY SYSTEMS, DESIGN, PUBLICATION, TESTING
 CODE 0003A

AUTH ANONYMOUS
 TITLE THE WARNE INFLATABLE OIL SPILLAGE BOOM
 PUBL WILLIAM WARNE AND CO., LTD.
 ABST A PICTORIAL SUPPLEMENT DESCRIBING THE WARNE BOOM.
 CODE 4014R

AUTH ANONYMOUS
 TITLE WARNE OIL SPILLAGE BOOMS
 PUBL SURFACE SEPARATION SYSTEMS
 ABST THIS ADVERTISEMENT DISCUSSES THE VARIOUS TYPES OF WARNE BOOMS AVAILABLE AS WELL AS SUGGESTED INSTALLATION TECHNIQUES.
 CODE 3005R

AUTH ANONYMOUS
 TITLE WASTE OIL RECOVERY PRACTICES STATE OF THE ART
 PUBL PRESENTATION OF EPA, DEC. 1974
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 REYN RECOVERY, WASTE DISPOSAL, LIQUID WASTES DISPOSAL
 CODE 0130A

AUTH ANONYMOUS
 TITLE WATERBURY DEBITS IN MARINE POLLUTION INCIDENTS
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 CODE 0780R

AUTH ANONYMOUS
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AUTH ANONYMOUS
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 ABST THIS ARTICLE ILLUSTRATES SOME OF THE WAYS THAT PHYSICISTS CAN HELP MEASURE AND CONTROL THE ENVIRONMENT - WAYS WHICH HAVE ESCAPED PHYSICISTS AND ENVIRONMENTALISTS ALIKE.
 REYN MEASURING U/L ON WATER, AIR POLLUTANTS, PHYSICISTS AND ENVIRONMENTALISTS
 CODE 2035R

AUTH ANONYMOUS
 TITLE THE WHY AND HOW OF UNDERSEA DRILLING
 PUBL AMERICAN PETROLEUM INSTITUTE
 ABST OUR UNWINDING OIL AND GAS SUPPLIES, THE POTENTIAL FOR INCREASING THESE RESERVES, AND THE ALTERNATIVES TO FINDING NEW DOMESTIC SOURCES OF PETROLEUM ARE DISCUSSED. WHY AND WHY WE MUST EXPLORE FOR AND PRODUCE FROM DEEPER OIL AND GAS NECESSARY TO PRESERVE THE NATIONAL, ECONOMIC, AND CONSUMER SECURITY OF THE UNITED STATES.
 REYN INCREASING RESERVES, EXPLORATION, PRODUCTION
 CODE 2088R

AUTH ANONYMOUS
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 PUBL OUL, 1973, 40 786-810
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AUTH ANONYMOUS
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 CODE 4003B

AUTH ANONYMOUS
 TITLE 1975 REPORT OF SPONSORED RESEARCH
 PUBL U.R.I.
 ABST EVERY SPONSORED RESEARCH PROJECT AT THE UNIVERSITY ACTIVE ON JULY 1, 1975 IS LISTED IN THIS BOOKLET UNDER THE NAME OF THE PROJECT'S PRINCIPAL INVESTIGATOR AND HIS OR HER COLLEGE.
 CODE 20424R

AUTH ANONYMOUS
 TITLE 1977 OIL SPILL CONFERENCE, PREVENTION BEHAVIOR, CONTROL, CLEANUP, MARCH 8-10, 1977
 PUBL NATIONAL CONVENTION CENTER
 ABST NEW TECHNIQUES AND EQUIPMENT BECA.
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 CODE 0197B

AUTH ANONYMOUS
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 ABST MARCH 19-22, 1974, LOS ANGELES, CALIFORNIA
 REYN PREVENTION, BEHAVIOR, CONTROL, CLEANUP
 CODE 7722C

AUTH ANONYMOUS
 TITLE 24 HOUR OIL SPILL CLEAN-UP SERVICE
 PUBL COASTAL SERVICES, INC.
 ABST OIL POLLUTION CONTROL AND CLEAN-UP SERVICE; HAZARDOUS MATERIALS SPILL CLEAN-UP SERVICE; WASTE OIL DISPOSAL
 CODE 4514R

AUTH ANONYMOUS
 TITLE 3000 HP ENDURANCE TEST OF THE DIESEL PRIME MOVER FOR ADAPTS
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. TR4101/004, MARCH 1974
 CODE 0744R

AUTH ANONYMOUS
 TITLE MODEL STUDY OF THE DILUTION OF SOLVABLE LIQUIDS DISCHARGES FROM TANKERS
 PUBL STEVENS INSTITUTE OF TECHNOLOGY, SEPT. 1973, 40 748-081
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AUTH ANONYMOUS
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 CODE 0221R

AUTH ANONYMOUS
 TITLE MEETINGS OF THE OIL-CONTINENTAL SHEET ENVIRONMENTAL STUDIES ADVISORY COMMITTEE
 PUBL DEPARTMENT OF THE INTERIOR, MAY 20-21, 1976
 ABST THIS MEETING COVERED THE ITEMS ON THE OFFICIAL AGENDA BUT NOT IN THAT SEQUENCE.
 REYN LEADING SCHEDULE, SALES, REVENUE
 CODE 2920R

AUTH ANTONI R.J.
 TITLE FEDERAL REGULATORY CONTROL OF OIL SPILL REMOVAL METHODS
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 ABST THE DEVELOPMENT OF FEDERAL REGULATORY CONTROLS FOR OIL REMOVAL METHODS IS TRACED.
 REYN REMOVAL, FEDERAL CONTROL, DEVELOPMENT
 CODE 0074R

AUTH APPEL B.A., MALL S.W., RESOLUTION J.J.
 TITLE FINAL REPORT - THE CHEMISTRY, DISPERSION AND TRANSPORT OF AIR POLLUTANTS EMITTED FROM FUELS IN POWER PLANTS IN CALIFORNIA
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 REYN FIELD MONITORING, PLUMES, AUTOMATIC SEQUENTIAL PARTICULATE SAMPLING
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AUTH API R.E., LEE V.J.
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 ABST THIS REPORT DOCUMENTS THE CY 1975 ENVIRONMENTAL MONITORING PROGRAM OF THE LOS ALAMOS SCIENTIFIC LAB. DATA ARE PRESENTED FOR CONCENTRATIONS OF RADIOACTIVITY MEASURED IN AIR, GROUND AND SURFACE WATERS, SEDIMENTS, SOILS AND FUNGUSSTUFFS AND ARE COMPARED WITH RELEVANT US ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION GUIDELINES.
 CODE 4178R

AUTH ARD R.W.
 TITLE COAST GUARDS RESPONSE TO SPILLED OIL
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 REYN MONITORING DETECTORS, SENSORS, RECOVERY
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AUTH BREHART-TREICHEL J.
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 PUBL SCIENCE NEWS, VOL. 102, NO. 26, OCT. 14, 1972
 ABST VARIOUS METHODS OF CLEAN UP ARE DISCUSSED.
 REYN CLEANUP, DISPENSANTS, TOXICITY
 CODE 2670R

AUTH ASPEN J.J., BOLLE P.
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 PUBL CONTROL TECHNOLOGY RESEARCH AND DEVELOPMENT
 ABST THE SYSTEM DESCRIBED IN THIS ARTICLE IS COMPOSED OF A ROTATING, MULTI-THREADED SCREW IN A CASING. THE OIL AND WATER ENTER THE SYSTEM AT A GIVEN SPEED

- AND ARE TRAPPED BETWEEN THE THREADS. THE PAPER ALSO DESCRIBES THE RELATED LABORATORY DEVELOPMENT WORK AND DATA ON THE PERFORMANCE OF THE DEVICE. REMOVAL, TERMINALS, ROTATING, MULTI-THREADED SCREW IN A CASING.
- KEYW 51231
- AUTH ATLANTIC RESEARCH SYSTEMS DIVISION
- TITL RECOVERY OF FLOATING OIL ROTATING DISK TYPE SKIMMER
- PUBL EPA, WATER QUALITY OFFICE, JULY 1973
- ABST DISCUSSES LABORATORY TESTS OF DISC MATERIALS. KEYW DISC MATERIALS, MULTIPLE DISCS, ROTATIONAL VELOCITY VECTOR
- CODE 0549F
- AUTH ATLAS R.W., BERTHA R.
- TITL DEGRADATION AND MINERALIZATION OF PETROLEUM BY TOL BACTERIA ISOLATED FROM COASTAL WATER
- PUBL BIOTECHNOL. BIOMENG., INT 297-308
- CODE 1035H
- AUTH ATLAS R.W., BERTHA R.
- TITL PATH AND EFFECTS OF POLLUTION PETROLEUM IN THE MARINE ENVIRONMENT
- PUBL RESOLVE REVIEWS VOL. 45
- CODE 0455A
- AUTH ATLAS R.W., MORWITZ A., BUSBY R.
- TITL PRUDHUE CRUDE OIL IN ARCTIC MARINE ICE, WATER AND SEDIMENT ECOSYSTEMS: DEGRADATION AND INTERACTION WITH MICROBIAL AND BENTHIC COMMUNITIES
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- ABST A VARIETY OF IN SITU MODELS WERE USED TO SIMULATE OIL SPILLS IN DIFFERENT ARCTIC ECOSYSTEMS. CONTAMINATION, ARCTIC, MICROORGANISMS
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- CODE 1034H
- AUTH AUDUNSON T., BRADENBURGH J.C., DALEN V.
- TITL STATUS AND RESULTS OF REMOTE SENSING ACTIVITIES AT THE CONTINENTAL SHELF INSTITUTE
- PUBL PRESENTED AT THE UCG OCEAN SYMPOSIUM IN REMOTE SENSING NOV. 2, 1978
- ABST THE CONTINENTAL SHELF INSTITUTE PARTICIPATES IN THE FIELD OF REMOTE SENSING BY STUDYING THE POSSIBILITIES FOR PRACTICAL APPLICATION OF REMOTE SENSING METHODS IN OCEANOGRAPHY AND MARINE GEOLOGY.
- KEYW REMOTE SENSING, MARINE GEOLOGY, SATELLITES
- CODE 7774F
- AUTH AYERS R.R.
- TITL A RIGID PERFORATED PLATE OIL BOOM FOR HIGH CURRENTS
- PUBL INDUSTRIAL ENVIRONMENTAL RESEARCH LAB., EPA, NO. 89-03-031, EPA 600/2-78-203, DEC. 1978
- ABST THIS REPORT DISCUSSES THE PERFORMANCE OF A NEW BOOM CAPABLE OF DIVERTING OIL SPILLS TOWARD SHORE IN A 3 ANCI RIVER OF TIDAL CURRENT.
- KEYW BOOMS, BAFFLES, FLOW RATES, TIDAL CURRENTS
- CODE 6199F
- AUTH AYERS R.R., PRASER J., BARRIENZA L.J.
- TITL DEVELOPING AN OPEN SEAS SKIMMER
- PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
- ABST DISCUSSES A SKIMMING SYSTEM DEVELOPMENT THAT SHOULD SOLVE MANY PROBLEMS WITH SKIMMING OIL IN OFFSHORE WATERS.
- KEYW OPEN-SEAS SKIMMER, "QUISCENT POOL", FLOW-DIFFUSING BAFFLE SYSTEM
- CODE 8554F
- AUTH BAGNOLD L.
- TITL SKIMMING APPARATUS
- PUBL OFFICIAL GAZETTE OF US PATENT OFFICE, VOL. 929, NO. 2.
- ABST DESCRIPTION OF A SKIMMING APPARATUS.
- CODE 3120A
- AUTH BAIER R.E.
- TITL ORGANIC FILMS ON NATURAL WATERS: THEIR RETRIEVAL, IDENTIFICATION AND MODES OF ELIMINATION
- PUBL JOURNAL OF GEOPHYSICAL RESEARCH, VOL. 77, NO. 27, SEPT 20, 1972
- ABST AIR-WATER INTERFACIAL FILMS WERE SAMPLED AND SUBJECTED TO NONDESTRUCTIVE ANALYSIS BY MULTIPLE ATTENUATED INTERNAL REFLECTION (MAIR) INFRARED SPECTROSCOPY.
- KEYW AIR WATER INTERFACE, SPECTROSCOPY, DEGRADATION
- CODE 7621F
- AUTH BAKER J.W., CRAPP G.B.
- TITL TOXICITY TESTS FOR PREDICTING THE ECOLOGICAL EFFECTS OF OIL AND EMULSIFICATION POLLUTION ON LITTORAL COMMUNITIES
- PUBL EGM. ASPECTS OF TOXIC TESTS OF OIL DISPERSANTS WORKSHOP, PHYL. INST. OF PL. LONDON, P. 24-46, 1974
- CODE 1062H
- AUTH BALDINI I., CUCUERA F.
- TITL ICHTHYOTOXIC EFFECTS OF SOME ANTI-POLLUTION PRODUCTS
- PUBL WATER RESEARCH VOL. 8, SP. 1973
- ABST A STUDY HAS BEEN CARRIED OUT ON THE ICHTHYOTOXICITY EFFECTS OF 14 ANTI-POLLUTION PRODUCTS USED FOR THE DISPERSION OF HYDROCARBONS IN WATER, ON THE CARASSIUS AURATUS. THE BETTER TOLERATED PRODUCTS ARE ESSOC LUBREXIT BOOE AND TOAN; POLLUTED BY FINE SOL US-72 AND SC WHILE THE OTHER PRODUCTS WERE FOUND TO CONTAIN HIGHER ICHTHYOTOXICITY CHARACTERISTICS.
- KEYW HYDROCARBONS, DISPERSANTS, TOXICITY, ICHTHYOTOXICITY
- CODE 7125F
- AUTH BALWAC B.C.
- TITL REPORT OF EL DONADO ASPHALT SPILL
- PUBL SOUTHEAST WATER LABORATORY, PAPA, AUG. 18, 1967
- ABST ON AUG. 18, 1967 THE BARCEL IS DONADO SPILL, SPILLING 225,000 GALLONS OF MASSES AND 103,000 GALLONS OF LIQUID ASPHALT. THIS PAPER DESCRIBES SUBSEQUENT REPAIR OPERATIONS ON THE BARGE AND A SERIES OF PHOTOGRAPHS DEPICTING THE SEVERAL OPERATIONS UNDERTAKEN IN ATTEMPTING TO DEAL WITH THE ASPHALT SLICK.
- CODE 3001R
- AUTH BARBER P.C.
- TITL CONTAINMENT OF OIL BY SEA ICE - SOME QUALITATIVE ASPECTS
- PUBL DIST. OF FISHERIES AND FORESTRY, OTTAWA, 1971
- KEYW CONTAINMENT, SEA ICE
- CODE 0266P
- AUTH BARBER P.C.
- TITL OIL SPILLS WITH ICE: SOME QUALITATIVE ASPECTS
- PUBL OIL SPILL PREVENTION
- ABST THIS PAPER GIVES AN INDICATION OF THE WAYS IN WHICH CONTAINMENT BY AN ICE COVER OF SPILLED OIL CAN OCCUR AND OF SOME OF THE WAYS IN WHICH THE CONTAINMENT MAY BE UTILIZED IN CLEANUP.
- KEYW CONTAINMENT, ICE COVER, CLEANUP
- CODE 0509F
- AUTH BARALUS W.W., BAUM J.S., ET AL.
- TITL INDUSTRIAL LIQUID WASTE CONTROL
- PUBL EDITORS REPRESENTING AMERICAN PETROLEUM INSTITUTE AND AMERICAN SOCIETY OF LUBRICATION ENGINEERS
- ABST THIS HANDBOOK IS INTENDED TO HELP INDUSTRY CONTROL OILY WASTES AND REDUCE THEIR COSTS. THE TECHNIQUES AND METHODS SUGGESTED ARE WELL ESTABLISHED AND PRACTICAL; THE INCENTIVES FOR DILIGENCE IN TERMS OF THE HIGH PENALTIES OF DELINQUENCY, ARE POWERFUL.
- KEYW OILY WASTE, CONTINENCY, TREATMENT.
- CODE 7770F
- AUTH BARBER W.H., GARNETT G.C.
- TITL ARTIFICIAL SEA SLICKS: THEIR PRACTICAL APPLICATIONS AND ROLE IN FUNDAMENTAL RESEARCH
- PUBL NIS, 410-780, JUNE 4, 1974
- ABST STUDY OF PRODUCTION AND USE OF ARTIFICIAL SLICKS.
- CODE 3118A
- AUTH BARBER W.H., GARNETT G.C.
- TITL EFFECTS OF AN ARTIFICIAL SEA SLICK UPON THE ATMOSPHERE AND THE OCEAN
- PUBL JOURNAL OF APPLIED METEOROLOGY VOL. 9, FEB. 1970
- CODE 2111A
- AUTH BARBER E., WIZENH J.
- TITL A GENERALIZED APPROACH TO THE FLUID DYNAMICS OF PARTICULATE SYSTEMS
- PUBL CANADIAN JOURNAL OF CHEMICAL ENGINEERING, VOL. 53, OCT. 1975
- ABST PART 2, SEDIMENTATION AND FLUIDIZATION OF CLOUDS OF SPHERICAL LIQUID DROPS. THIS PAPER DISCUSSES THE INTERACTION BETWEEN SLICK SPHERICAL PARTICLES DURING SEDIMENTATION.
- KEYW SLICK SPHERICAL PARTICLES, SEDIMENTATION, FLUIDIZATION
- CODE 6328F
- AUTH BARNETT C.J., KONTOGIANNIS J.E.
- TITL THE EFFECT OF CRUDE OIL FRACTIONS ON THE SURVIVAL OF A TIDEPOOL COPEPOD, TIGRIDOPUS CALIFARNICUS
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- ABST THE EFFECT OF FOUR CRUDE OIL FRACTIONS ON THE SURVIVAL OF A TIDEPOOL COPEPOD WERE STUDIED.
- CODE 3096R
- AUTH BART D.L.
- TITL GULF ASSOCIATES: THE ORGANIZATION AND CAPABILITIES OF AN OIL SPILL CLEANUP ASSOCIATION FOR THE GULF OF MEXICO
- PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1999, MAY 4-8, 1974
- CODE 0375H

- AUTH BARTLETT E.S., MAWU R.A.
 TITLE METHODOLOGY FOR ASSESSING ENVIRONMENTAL IMPLICATIONS AND TECHNOLOGIES: NONFERROUS METALS INDUSTRIES
 PUBL ENVIRONMENTAL PROTECTION TECHNOLOGY SERIES, EPA-600/2-70-303, DEC. 1970, 68-02-1322, PG. 54
 ABST THE SUBJECT OF THIS REPORT IS THE DEVELOPMENT OF METHODOLOGY FOR MAINTAINING AWARENESS OF THE ENVIRONMENTAL IMPLICATIONS OF NONFERROUS METALS TECHNOLOGY.
 REYN NONFERROUS METALS, METHODOLOGY, AWARENESS SYSTEM
 CODE 0510F
- AUTH BARTLETT S.F.
 TITLE IN-SITU MEASUREMENTS OF OIL BARRIER SHAPES, LOADS AND MOTIONS
 PUBL THESIS FOR MASTER OF SCIENCE IN OCEAN ENGINEERING, UM1, 1973
 ABST A STUDY INVESTIGATING THE SHAPE, LOADING AND MOTIONS OF A COMMERCIALY PRODUCED PHYSICAL GEL BUMP IN ORDER TO OBTAIN ADDITIONAL INFORMATION USEFUL TO MARINE DESIGN.
 CODE 0037H
- AUTH BASCL D.P.
 TITLE PNEUMATIC BARRIERS FOR OIL CONTAINMENT UNDER WIND, WAVE AND CURRENT CONDITIONS
 PUBL PHYSICAL REMOVAL
 ABST THIS PAPER REPORTS ON THE EFFECTIVENESS OF THE PNEUMATIC BARRIERS FOR OIL CONTAINMENT UNDER WIND, WAVE AND CURRENT CONDITIONS.
 REYN PREVENTION, PNEUMATIC BARRIERS, BUBBLE-GENERATED CURRENT
 CODE 0870F
- AUTH BATES C.C., VOST P.
 TITLE WINDS TRENDS THE FLAG OF POLLUTANT SHIPS? LAW OF THE SEA: THE EMERGING REGIME OF THE OCEANS, 1974
 ABST DISCUSSES RELATIVE TREAT OF SHIP SOURCE POLLUTION, CONTAINS MANY AND PAREL STATISTICS PERTAINING TO THIS.
 CODE 3101H
- AUTH BATTILLE INDUSTRIAL INSTITUTE
 TITLE CONCEPT DEVELOPMENT OF A HYDRAULIC SKIMMER SYSTEM FOR RECOVERY OF FLOATING OIL
 PUBL EPA, WATER QUALITY OFFICE, APRIL 1971
 ABST DISCUSSION OF A HYDRAULIC SKIMMER AS AN EFFECTIVE COUNTERMEASURE AGAINST FLOATING OIL SLICKS.
 REYN CONCEPT, EQUIPMENT DEVELOPMENT, OIL SKIMMER, OPEN SEAS
 CODE 0520F
- AUTH BAUER H.A., FULLERT J.J.
 TITLE CHEMICAL ADDITIVES TO CONTROL OIL SPILLS - A STATE-OF-THE-ART SURVEY
 PUBL BENSSELAIR POLYTECHNIC INSTITUTE, 60-7705ST, JAN. 1974
 ABST UP-TO-DATE USES OF CHEMICALS IN OIL SPILLS, INCLUDES EXTENSIVE BIBLIOGRAPHY
 CODE 3132H
- AUTH BAUMEISTER R.J., MARILL T.D.
 TITLE LIQUID DROPS: NUMERICAL AND ASYMPTOTIC SOLUTIONS OF THEIR SHAPES
 PUBL NATIONAL AERONAUTICS AND SPACE ADMINISTRATION, NASA TN D-4179
 ABST THE SHAPES OF LIQUID DROPS RESTING ON FLAT SURFACES WERE DETERMINED BY A RUNGE-KUTTA SOLUTION OF THE LAPLACE CAPILLARY EQUATION. A CHARACTERISTIC LENGTH EQUAL TO THE SQUARE ROOT OF SURFACE TENSION DIVIDED BY THE PRODUCT OF DENSITY AND GRAVITY WAS USED TO NONDIMENSIONALIZE THE NUMERICAL RESULTS. IN ADDITION, ASYMPTOTIC SOLUTIONS FOR SMALL AND LARGE DROPS WERE OBTAINED TO GIVE EXPLICIT EXPRESSIONS FOR THE MAXIMUM DROP HEIGHT AND RADIUS. THESE CORRELATIONS APPLY FOR THE COMPLETE RANGE OF LIQUID VOLUMES & CONTACT ANGLES.
 REYN NUMERICAL SOLUTIONS, DROP VOLUME, LIQUID DROPS
 CODE 7737H
- AUTH BAYRENT B.
 TITLE ANALYSIS OF OIL SPILL ACCIDENTS FOR ENVIRONMENTAL IMPACT STATEMENTS
 PUBL STANDARD OIL CO. OF CAL.
 ABST THIS PAPER DESCRIBES A COMPREHENSIVE APPROACH TO ANALYSIS OF OIL SPILL ACCIDENTS IN ENVIRONMENTAL IMPACT STATEMENTS. IT IDENTIFIES SOURCES OF RELEVANT DATA AND TECHNICAL INFORMATION WHILE ALSO POINTING OUT AREAS WHERE KNOWLEDGE IS INCOMPLETE. ACCIDENTS, TECHNICAL INFORMATION, RELEVANT DATA, ENVIRONMENTAL IMPACT STATEMENTS
 CODE 0075H
- AUTH BECKER P.
 TITLE EMULSIONS - THEORY AND PRACTICE - SECOND EDITION
 PUBL REINOLD PUBLISHING CORP.
 ABST THIS BOOK IS AN ESSENTIALLY SELF-CONTAINED DISCUSSION OF MODERN EMULSION THEORY AND PRACTICES, WITH PARTICULAR ATTENTION TO THE DEVELOPMENT OF THE LAST PATTERN IN SEVENTEEN YEARS.
 REYN EMULSIONS, THEORY AND PRACTICES, DEVELOPMENT
 CODE 2065H
- AUTH BECKER C.D., LICHTENICER J.A., SCHNEIDER R.J., STRANG J.A.
 TITLE REGIONAL SURVEY OF MARINE BIOTA FOR BIODIVERSITY STANDARDIZATION OF OIL AND OIL DISPERSANT CHEMICALS
 PUBL APL COMMITTEE ON ENVIRONMENTAL AFFAIRS, NO. 4107, APR. 6, 1973
 ABST THIS REPORT SURVEYS EFFECTS ON ENVIRONMENT OF OIL DISPERSANTS.
 REYN DISPERSANTS, ENVIRONMENTAL EFFECT, MARINE BIOTA
 CODE 2055F
- AUTH BELLAN G.L.
 TITLE THE SUB-LETHAL EFFECTS OF A DETERGENT ON THE REPRODUCTION, DEVELOPMENT AND SETTLEMENT IN THE POLYCHAETOUS ANNELO
 PUBL MAR. BIOL. 16:103-108, 1972
 CODE 1011H
- AUTH BELLAN G.L.
 TITLE TOXICITY TESTING AT THE STATION MARINE D'ENDAUVE
 PUBL BAYMON, L.R. AND CORWELL E. EDITORS, ECOLOGICAL ASPECTS OF TOXICITY TESTING OF OILS AND DISPERSANTS, EPREL. OF A WORKSHOP, PP 63-67, BRISTOL, ESSEA, APPLIED SCIENCE PUBLISHERS
 CODE 1010H
- AUTH BENZER R.W.
 TITLE A STUDY OF THE BIOLOGICAL EFFECTS OF OIL POLLUTION AND THE EFFECTS OF ITS REMEDY
 PUBL SENIOR PROJECT MAY 1972
 ABST THE OBJECTIVE OF THE RESEARCH IS TO DETERMINE HOW SEVERE THE PROBLEMS OF OIL POLLUTION ARE AND WHETHER OR NOT THE EFFORT OF THEIR SOLUTION CAN BE LOOKED UPON IN A DIFFERENT LIGHT.
 CODE 3070H
- AUTH BERGLUND M.
 TITLE INFLUENCE OF WETTING AGENTS ON GROWTH OF MARINE MULTICELLULAR GREEN ALGAE
 PUBL WATER, 2: 157-165
 CODE 1004H
- AUTH BERNARD M., JAKOBSEN A.
 TITLE EFFECTIVENESS OF DEVICES FOR THE CONTROL AND CLEANUP OF OIL SPILLS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1523, MAY 1-3, 1972
 ABST A REVIEW OF THE CONTAINMENT AND CLEANUP METHODS EMPLOYED DURING THE CHEVRON AND SHELL INCIDENTS IN THE GULF OF MEXICO IS PRESENTED.
 REYN CONTAINMENT, ADSORBENT SYSTEMS, CLEANUP
 CODE 0901F
- AUTH BERNICKE S., THOMAS M., CLARKE A.
 TITLE THE FORMATION AND STABILITY OF EMULSIONS OF WATER IN CRUDE PETROLEUM AND SIMILAR SITUATIONS
 PUBL PAPER PRESENTED AT THE INSTITUTE OF PETROLEUM IN THE SCIENTIFIC ASPECTS OF POLLUTION OF THE SEA BY OIL, OCT. 1968
 CODE 5001H
- AUTH BERNHARDT S.A., DEAN A.A., FALLOUS N.G., FISH A.
 TITLE THE PROPERTIES OF PERSISTENT OIL AT SEA
 PUBL UNKNOWN
 ABST THIS PAPER DISCUSSES THE PHYSICAL, CHEMICAL, AND BIOLOGICAL PROCESSES WHICH MAY OPERATE ON LARGE OIL AFTER A SPILL AT SEA.
 REYN REMOVAL, DISPERSION, PROPERTIES OF OIL
 CODE 0870F
- AUTH BERRY G.L., HOLBE J.W.
 TITLE CLEAN GULF ASSOCIATES UNVEILS A NEW GENERATION OF OIL SPILL CLEAN-UP EQUIPMENT
 PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
 ABST THE ORGANIZATION AND CAPABILITIES OF CLEAN GULF ASSOCIATES ARE REVISED, NEW EQUIPMENT, ADDITIONS AND IMPROVEMENTS TO EXISTING ITEMS ARE DESCRIBED.
 REYN CONTAINMENT, CLEANUP
 CODE 0920F
- AUTH BETTS W.E.
 TITLE CLEANUP OF INLAND OIL SPILLS
 PUBL APPLIED CENTRAL TECHNOLOGY
 ABST THIS PAPER OUTLINES THE REQUIREMENTS WITH DEALING WITH ACCIDENTAL INLAND SPILLS.
 REYN CLEANUP, DEVELOPMENT OF EQUIPMENT, HYDRAULIC DRIVE SYSTEMS
 CODE 0905F
- AUTH BETTS W.E.
 TITLE INLAND OIL SPILL - CLEANUP MANUAL
 PUBL 0350 - ENVIRONMENTAL CONSERVATION
 ABST THIS DOCUMENT DESCRIBES THE BEHAVIOR OF OIL WHEN IT IS SPILLED ON THE GROUND, WHEN IT PENETRATES BELOW GROUND, REACHES GROUND WATER OR WHEN IT IS ON INLAND AND SHELTERED SURFACE WATER OF ALL TYPES. CLEAN UP METHODS APPROPRIATE TO EACH SITUATION ARE CONSIDERED.
 REYN CLEANUP, PREVAILING CONDITIONS, CONFINEMENT
 CODE 2060F
- AUTH BETTS W.E., FULLER M.L., JAGGER M.
 TITLE AN INTEGRATED PROGRAM FOR OIL SPILL CLEANUP
 PUBL OIL SPILL CLEANUP
 ABST THIS PAPER DISCUSSES THE NECESSARY REQUIREMENTS OF

AN INTEGRATED PROGRAM FOR DEALING WITH OIL SPILLS ON WATER.
 CLEAN UP, ORGANIZATION, EQUIPMENT AND MATERIALS
 KEYW
 CODI 0621F

AUTH BEYNON L.A.
 TITLE CLEANING UP
 PUBL MARUSPILL MARCH 1968
 ABST DEALS WITH LESSONS LEARNED AS A RESULT OF THE GROUNDING OF THE OIL TANKER TORREY CANYON. THE AUTHOR WAS PRESENT AT THE CLEANING UP OPERATIONS.
 CODE 0024R

AUTH BEYNON L.A.
 TITLE EVALUATION OF DISPERSANTS
 PUBL BRITISH PETROLEUM CO. RESEARCH AND TECHNICAL DEVELOPMENT DEPT. LONDON, CITATION NO. P70-04374, 1965
 CODE 1115H

AUTH BEYNON L.A.
 TITLE OIL SPILL DISPERSANTS. WORKSHOP ON OIL SPILL CLEAN-UP
 PUBL JOURNAL OF THE INSTITUTE OF PETROLEUM, VOL. 57, JAN. 1971
 ABST THIS PAPER DISCUSSES EFFECTIVENESS OF DISPERSANTS ON OIL SPILL CLEANUP.
 KEYW CLEANUP, DISPERSANTS
 CODE 2134F

AUTH BEYNON L.A., CONNELL E.B.
 TITLE ECOLOGICAL ASPECTS OF TOXICITY TESTING OF OILS AND DISPERSANTS
 PUBL UNPUBLISHED PRESS WORK
 ABST THIS BOOK CONTAINS THE PROCEEDINGS OF A WORKSHOP CONVENED BY THE INSTITUTE OF PETROLEUM, LONDON. THE MEETING WAS HELD TO REVIEW TOXICITY TESTING RESEARCH IN EUROPE AND TO DISCUSS CRITICALLY THE MANY PROBLEMS THAT HAVE BEEN EXPERIENCED BY LEADING NATIONS IN THE FIELD.
 KEYW OIL, DISPERSANTS, TOXICITY TESTING
 CODE 0147D

AUTH BEYNON L.A., LESTER T.E., BROCKIS C.J., HOLMES P.D.
 TITLE PLANNING AND DEVELOPING A COMPANY OIL SPILL CONTINGENCY PLAN
 PUBL B.P. TRADING LTD.
 ABST THERE ARE THREE KEY COMPONENTS TO THIS PLAN: 1. THE ORGANIZATION OF A HAZARDOUS SCHEME, 2. THE CHOICE AND PURCHASE OF EQUIPMENT, 3. THE IDENTIFICATION, NOMINATION AND TRAINING OF PERSONNEL
 KEYW CONTINGENCY, TRAINING, PLANNING, DEVELOPING, PERSONNEL
 CODE 0103H

AUTH BEZONI A.M.
 TITLE POLLUTION RESPONSE/EFFECTS OF WAVES ON OIL SPILL MOVEMENTS
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 CODE 0435P

AUTH BIANCHI R., JOHANSON E., PARRELL J.
 TITLE THE APPLICATION OF SWIMMERS, PISTON FILMS, AND SORBENTS FOR OPEN WATER SPILLS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1740, APR. 29 - MAY 2, 1973
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 KEYW CLEANUP, SWIMMERS, PISTON FILMS, SORBENTS, BOSTON HARBOR
 CODE 5121F

AUTH BIANCHI R., PARRELL J., JOHANSON E.
 TITLE DEMONSTRATION OF FIRED AND MOVING INCLINED PLANE OIL SWIMMERS FOR COLLECTING OIL UNDER THE WATER SURFACE
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 KEYW REMOVAL, SWIMMERS, INCLINED PLANE
 CODE 0831F

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 TITLE USE OF THE MASSACHUSETTS DIP OIL SWIMMER ON FREE SLICES IN THE CASCO BAY (PORTLAND) SPILL
 PUBL APPLIED CONTROL TECHNOLOGY
 ABST THIS PAPER DISCUSSES THE NECESSITY OF TESTING AN OPERATING PLAN ESPECIALLY AS IT RELATES TO THE CLEANUP HARDWARE TO BE USED.
 KEYW CONTAINMENT, CLEANUP, SWIMMING, MOBILE STORAGE
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AUTH BIANCHI R.A., HENRY G.
 TITLE THE DEVELOPMENT AND DEMONSTRATION OF AN UNDERWATER OIL HARVESTING TECHNIQUE
 PUBL EPA, 82-73-203, NTIS-11063, APR. 1973
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AUTH BIANCHI R.A., JOHANSON E., PARRELL J.M.

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AUTH BIGNARD R.
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 PUBL ERDA
 ABST REPORT ON THE JOB OF AN OIL SPILL FIGHTER
 CODE 2044R

AUTH BIGNARD R.E.
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 PUBL EPA
 ABST THE U.S. POLICY ON THE USE OF CHEMICAL DISPERSANTS TO REMOVE OIL SPILLS IN NAVIGABLE WATERS.
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 CODE 2002F

AUTH BIRNS A.F.
 TITLE DETERMINATION OF OIL EFFLUENT GUIDELINE FOR INDUSTRIAL DISCHARGES IN THE STATE OF NEW JERSEY: IS 1 PPM REALISTIC AND OBTAINABLE
 PUBL STATE OF NJ, DEPT. OF ENVIRONMENTAL PROTECTION FOR EPA 1975 CONFERENCE
 ABST THIS PAPER SETS FORTH CRITERIA FOR THE ESTABLISHMENT OF A MAXIMUM LIMIT OF 1 PPM OIL IN A DISCHARGE
 KEYW DETERMINATION, OIL EFFLUENT GUIDELINE, INDUSTRIAL DISCHARGES, NEW JERSEY, 1 PPM
 CODE 0070R

AUTH BLACK J.
 TITLE PREVENTION OF SPILLAGE AT MOORING TERMINALS
 PUBL TANKER AND BULK CARRIER 2015:1 20-30-32
 CODE 0320H

AUTH BLACK R.B.
 TITLE CURRENT STATUS OF ALTERNATIVE DEEPWATER TERMINAL FEASIBILITY STUDIES
 PUBL UNPUBLISHED
 ABST THIS STUDY, WHICH COVERS THE THREE CLASSES INCLUDES MOVEMENT FORECASTS AND ANALYSIS OF ENVIRONMENTAL PROTECTION AND SHIPPING COSTS FOR BOTH LIQUID AND DRY BULK COMMODITIES.
 KEYW DEEPWATER TERMINALS, FOREIGN TRADE, TERMINAL LOCATION
 CODE 7190F

AUTH BLACKMAN R.P.
 TITLE TOXICITY OF OIL SINKING AGENTS
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 CODE 1041H

AUTH BLAIR E., COE J., RUD L.
 TITLE FINAL REPORT - INVESTIGATION OF FLUSHING TIME ON THE LAFAYETTE RIVER, NURFOLA, VA.
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AUTH BLEAKLEY A.J., BAUDEN J.S.
 TITLE EFFECTS OF AN OIL SPILL REMOVER ON BEACH MICROFLORA
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AUTH BLOKOWICH T.W.
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 ABST THIS REPORT PRESENTS THE RESULTS OF THE AT-SEA TESTS CONDUCTED ON THE OCEAN SYSTEMS, INC. RECOVERY, CURRENT SPEEDS, TOWLINE LOADS, PUMPING RATES, WAVE HEIGHTS
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- AUTH BLOOM S.A.
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POLLUTION
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- AUTH BLUMER R.
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- AUTH BURNS A., MCCRAY D., SHIU M.T.
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UNIVERSITY OF TORONTO, TORONTO, ONTARIO, CANADA
ABST THIS PAPER ADDRESSES THE PROBLEM OF CALCULATING
THE DISTRIBUTION OF SPECIFIC HYDROCARBONS BETWEEN
THE OIL PHASE, THE AQUEOUS PHASE AND THE MUD
PHASE DURING A TOXICITY TEST. THIS MAY BE AN
ESSENTIAL COMPONENT OF INTERPRETING THE TOXICITY
OBSERVATIONS.
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- AUTH BOEHM P.D., QUINN J.C.
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- AUTH BONE P.L.
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- AUTH BROMS J.A., SACKETT G.W.
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- AUTH BROWN C., LYNCH P.
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WHICH HAD BEEN IN THE MARINE ENVIRONMENT FOR 2-7
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- AUTH BROWN C., LYNCH P., AMRADIAN M.
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KEYW DISPERSANTS, HYDROCARBONS, RUBBIT LAKE
CODE 70188
- AUTH BROWN C.W.
TITL URI CHEMISTS DEVELOP A FAST, SURE METHOD OF
IDENTIFYING THE SOURCES OF OILSPILLS
PUBL MARITIME, VOL. 17, NO. 4, AUG. 1973
ABST THIS PAPER DISCUSSES A SPECTROSCOPIC
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THAT APPROPRIATE SOFTWARE CAN BE WRITTEN WITHOUT
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- AUTH BROWN G., JASPER B.
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- AUTH BROWN G.A., JASPER B., BONDILL R., STRAIN T.,
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 CODE 2950F
- AUTH BROWN G.A., LARRABEE R.M.
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- AUTH BROWN P.E.
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 REYN CALIBRATION TECHNIQUES; REMOTE SENSING; BIBLIOGRAPHY
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- AUTH BAUCH B., MARSHALL R.P.
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 PUBL J. MARINE BIOLOGICAL ASSOCIATION U.K., VOL. 49, NO. 4, 1969
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- AUTH BULTMAN J.D., LEONARD J.M.
 TITLE OCEAN SURFACE FILMS MAY-JUNE 1963
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 CODE 6052F
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- AUTH BURKIN C.E., CULLEY J.D., OREN M.L.
 TITLE BACKGROUND INFORMATION ON HYDROCARBON EMISSIONS FROM MARINE TERMINAL OPERATIONS
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 REYN MARINE TERMINALS, HYDROCARBONS, EMISSIONS
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- AUTH BURWOOD R., SPEERS G.C.
 TITLE PHOTODUPLICATION AS A FACTOR IN THE ENVIRONMENTAL IMPACT OF CRUDE OIL ESTUARINE AND COASTAL MARINE SCIENCES
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- AUTH BUTLER J.A.
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- AUTH BUTLER J.A., SEVY E.P.
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- AUTH CADY G.
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 CODE 2952F
- AUTH CAHNS R.
 TITLE OIL SPILL REPORT
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 ABST THIS ARTICLE CONCERNS THE WRECK OF THE T-HEWIT CANTON AND THE OCEAN EAGLE. IT IS AN ATTEMPT AT AN OBJECTIVE REPORT ON THE MAJOR OIL SPILLS IN RECENT YEARS, THEIR CAUSES AND EFFECTS, AND WHAT WE HAVE LEARNED ABOUT DEALING WITH SUCH INCIDENTS, ACCIDENTS, CAUSES, AND EFFECTS
 REYN
 CODE 3039F
- AUTH CALABRESI A., DAVIS M.C.
 TITLE EFFECTS OF SOFT DETERGENTS ON EMBRYOS AND LARVAE OF AMERICAN OYSTER
 PUBL PROC. NATL. SHELLFISH ASSOC., VOL. 57, 1967
 CODE 1001F
- AUTH CAMPBELL F.J.
 TITLE STANDARDIZED HARDWARE FOR OIL SPILL CONTAINMENT BOOMS
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 ABST THIS REPORT DESCRIBES THE DESIGN, DEVELOPMENT AND TESTING OF STANDARDIZED HARDWARE FOR USE WITH EXISTING AND NEW NAVAL OIL SPILL CONTAINMENT BOOMS.
 REYN CONTAINMENT, REMOVAL, BOOMS
 CODE 0521F
- AUTH CAMPBELL F.J., MARTIN S.
 TITLE OIL AND ICE IN THE ARCTIC OCEAN POSSIBLE LARGE-SCALE INTERACTION
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- AUTH CANEVARI C.
 TITLE GENERAL DISPERSANT METHOD
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- AUTH CANVARI C.
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- AUTH CONEYARI G.P.
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- AUTH CONEYARI G.P.
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- AUTH CONEYARI G.P.
 TITL DEVELOPMENT OF THE "NEXT GENERATION" CHEMICAL DISPERSANTS
 PUBL PROCEEDINGS OF THE 1973 CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS, MARCH 13-15, 1973
 ABST REVIEW OF CURRENT STATUS OF CHEMICAL DISPERSANTS IN ORDER TO DEVELOP FUTURE DISPERSANTS.
 KEYW DISPERSANTS, CONTROL TOXICITY
 CODE 5043F
- AUTH CONEYARI G.P.
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 ABST THIS PAPER REVIEWS SOME OF THE PAST HISTORY AS BACKGROUND IN ORDER TO DEFINE THE PROS AND CONS REGARDING THE USE OF DISPERSANTS.
 KEYW DISPERSANTS, EFFECTIVENESS, TOXICITIES
 CODE 5049F
- AUTH CONEYARI G.P.
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 KEYW LUMP ON TOP, CHEMICAL DISPERSANTS, CONTAINMENT, RECOVERY, TREATMENT
 CODE 5126F
- AUTH CONEYARI G.P.
 TITL SOME BASIC CONCEPTS REGARDING THE SEPARATION OF OIL WATER MIXTURES
 PUBL ASME TRANSACTIONS, 12(13) JULY 1964
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- AUTH CARU J.C., PONCE P.V., SNIDER R.D.
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 ABST INFORMATION HAS BEEN COLLECTED ON 3,715 WORLD-WIDE TANKSHIP ACCIDENTS INVOLVEMENTS DURING THE PERIOD 1964-1973 FROM LLOYD'S MARINE CASUALTY REPORTS AND OTHER SOURCES. INFORMATION COLLECTED, ONCE ANALYZED, SHOULD BE USEFUL IN EVALUATING MEASURES FOR REDUCING ACCIDENTS AND RESULTING OIL OUTFLOWS.
 KEYW ACCIDENTS, TANKERS, OIL OIL FLOWS
 CODE 0095H
- AUTH CARRICHAEL P.R.
 TITL OFFSHORE DRILLING TECHNOLOGY
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 ABST THIS BOOK SUPPLIES DETAILED TECHNICAL INFORMATION AND ADVANCED TECHNICALLY ORIENTED REVIEW OF OFFSHORE DRILLING TECHNIQUES AND APPARATUS.
 KEYW OFFSHORE DRILLING, TECHNIQUES, APPARATUS
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- AUTH CARPENTER C.E., BUTCHER L.F., MURLEY A.S.
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 CODE 2807F
- AUTH CARTER H.W., SCHMEL J.R., MILSON R.E., WOODHEAD P.H.
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- AUTH CARTY J.D., ARTHUR D.
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- AUTH CASCIUINE P.
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- AUTH CATO C.
 TITL THE APPLICABILITY OF REMOTE SENSING TECHNIQUES FOR OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1006, MAY 1-3, 1972
 ABST IN THIS REPORT A COMPREHENSIVE SURVEY OF THE STATE-OF-THE-ART OF VARIOUS REMOTE SENSING TECHNIQUES THAT HAVE USE OF BOTH SPECTRAL AND THE SPATIAL DIMENSIONS OF REMOTE SENSING ARE GIVEN. DETECTION, IDENTIFICATION, THICKNESS, MAPPING, SENSING TECHNIQUES
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- AUTH CHAMBERS B.E., WILLIAMS M.U.
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- AUTH CHAN G.L.
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 KEYW EFFECTS SAN FRANCISCO OIL SPILL, MARINE LIFE, RECRUITMENT
 CODE 0344H
- AUTH CHANG H., SAMER E.W.
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 ABST THIS PAPER DISCUSSES THE EVALUATION OF FOUR PHOTOGRAPHIC THIN FILM OIL SAMPLERS FOR USE IN SAMPLING FOR IDENTIFICATION PURPOSES.
 KEYW DEPLOYMENT, RETRIEVAL, CLEANING
 CODE 0054F
- AUTH CHAPIN A.L.
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- AUTH CHARLTON T.J., CUMMINGHAM J.R.
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 ABST THE OIL SPILL PREVENTION PROGRAM OF THE EPA IS DISCUSSED AS IT HAS EVOLVED FROM THE IMPLEMENTING LEGISLATION. THE PAPER DISCUSSES EPA PLAN REVIEWS, AMENDMENT PROCEDURES, APPEALS ON AMENDMENTS, AND PENALTY PROCEDURES AND APPEALS FOR PENALTIES.
 KEYW PREVENTION, LEGISLATION, PENALTIES
 CODE 0001H
- AUTH CHARENCA M.
 TITL WIND STRESS ON A WATER SURFACE
 PUBL UNMANNED
 ABST THIS REPORT SUMMARIZES THE RESULTS OF TESTS OF WIND STRESS ON A WATER SURFACE.
 KEYW WIND PROPELLER, AERODYNAMICS, PRECISION ANEMOMETRY
 CODE 0423F
- AUTH CHEN E.C., EVERALL J.L., PHILLIPS C.R.
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- AUTH CHUNG J.S.
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 ABST THIS PAPER DISCUSSES OIL THICKNESS AND ITS VARIATION DETERMINING A DESIGN REQUIREMENT FOR THE AUTUMN CHARACTERISTICS OF THE CONTROL EQUIPMENT IN WAVES
 KEYW WIND EFFECT, OIL LAYER THICKNESS, SPREADING
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- AUTH CHUNG J.S., EVAN J.R., CUMMINGHAM J.R.
 TITL DESIGN PARAMETER STUDY OF AN OIL SPILL BOOM
 PUBL CONTROL TECHNOLOGY RESEARCH AND DEVELOPMENT
 ABST THIS PAPER PRESENTS A DESIGN PARAMETER STUDY OF AN OIL SPILL CONTAINMENT BOOM.
 KEYW CONTAINMENT CONTROL, BOOM
 CODE 0520F

- AUTH CUMMINGS R.J.
 TITLE PHOTOGRAPHIC TECHNIQUES FOR CHARACTERIZATION AND MONITORING OIL AND WASTE STREAMS
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 CODE 0076
- AUTH LINDBERG R., HANN S., STRAUGHAN U.
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 PUBL UNIV. OF CALIF., 1973 CONF.
 ABST THIS ANALYSIS INDICATES THAT SAND MOVEMENT AND SUBSTRATE STABILITY ARE THE TWO MOST IMPORTANT FACTORS AFFECTING THE PRESENCE OF MARINE ORGANISMS ON THESE BEACHES DURING THIS TIME.
 CODE 0177
- AUTH CLARA R.D.
 TITLE OIL-LEAKING RESCUE AND CONSERVATION
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 REYN OIL-LEAK RESCUE, CONSERVATION, WATER-REPELLENT PLUMAGE
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- AUTH CLARA R.D., FINLEY J.S.
 TITLE PARAFFIN HYDROCARBON PATTERNS IN PETROLEUM POLLUTED MUSSELS
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 CODE 1071
- AUTH CLARA R.D., FINLEY J.S., PATTEN D.C., DENIAL E.L.
 TITLE LOW TEMP CHEMICAL AND BIOLOGICAL EFFECTS OF A PERSISTENT OIL SPILL INCLUDING THE GROUNDING OF THE GENERAL M.C. REIGUS
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 REYN CHEMICAL AND BIOLOGICAL EFFECTS, GENERAL M.C. REIGUS, GROUNDING
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- AUTH CLARA R.D., PATTEN D.C., DENIAL E.L.
 TITLE OBSERVATIONS OF A COLD WATER INTERTIDAL COMMUNITY AFTER FIVE YEARS OF A LOW-LEVEL, PERSISTENT OIL SPILL FROM THE GENERAL M.C. REIGUS
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 ABST THIS ARTICLE DISCUSSES THE OBSERVATIONS OF A TIDAL COMMUNITY AFTER AN OIL SPILL.
 REYN HYDROCARBONS, PETROLEUM CONTAMINATION BIOLOGICAL EFFECTS
 CODE 2009
- AUTH CLYNE R.W.
 TITLE MECHANICAL RETRIEVAL OF WASTE OIL AND SOLIDS FROM WATER
 PUBL OCEAN EQUIPMENT COMPANY, MAY 6, 1968
 ABST THIS PAPER DISCUSSES THE APPLICATION OF ROTATING CYLINDERS FOR THE RECOVERY OF OIL SPILLS FROM INLAND WATERWAYS AND PROTECTED HARBORS, AND FOR THE RETRIEVAL OF WASTE OILS FROM WASTE WATER. IT ALSO DISCUSSES THE GENERAL DESIGN DETAILS OF PERMANENT FIBRE-REINFORCED OIL RETENTION FLOATING BLOKS FOR MARINE AND INDUSTRIAL APPLICATION.
 CODE 3014
- AUTH ECKHART G.F.
 TITLE IN SITU STUDIES OF THE SEASONAL SUCCESSIONAL TRAJECTORIES OF TRANSPLANTED AND EXPERIMENTAL DIATOM ASSEMBLAGES
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 ABST THIS PAPER DISCUSSES INVESTIGATIONS FOCUSED ON INTERPRETING THE SIGNIFICANCE OF ALTERATIONS IN COMMUNITY STRUCTURE.
 REYN DIVERSITY, RESILIENCE STABILITY, PERSISTENCE OF COMMUNITIES
 CODE 0077
- AUTH COCHRAN B.A., PRASER J.P.
 TITLE COMPUTER SIMULATION OF OFFSHORE OIL SPILL CLEANUP OPERATIONS
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 REYN COMPUTER SIMULATION, RECOVERY, SWIMMERS
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- AUTH COCHRAN B.A., HANNEY G.A.
 TITLE COMPUTER SIMULATION OF OFFSHORE OIL-SPILL CLEANUP OPERATIONS
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- AUTH COCHRAN B.A., SCOTT P.R.
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 REYN SURFACTANTS, CLEANUP, PREDICT BEHAVIOR, DISPERSANTS
 CODE 2515F
- AUTH COLBURN D.E.
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 PUBL USCG, DEPT. OF TRANSPORTATION, REPORT NO. CG-0-33902-4-2, SEPT. 1973
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- AUTH COLBURN D.E., MIDDLETON F.M., LEBLANC L.R.
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- AUTH COLE M.A.
 TITLE MOVEMENT OF OIL SLICKS INCLUDING PREDICTION
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- AUTH CULE T.J.
 TITLE PRELIMINARY ECOLOGICAL-GENETIC COMPARISON BETWEEN UNPERTURBED AND OIL IMPACTED LINGULIDAE GENERA (PROSOBRANCHIATA: GASTROPODA) POPULATIONS: NUBSHA POINT (WOODS HOLE) AND WILD HARBOR (WEST PALMOUTH), MASSACHUSETTS
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- AUTH COLWELL R.A., MILLS A.L., WALKER J.D., GARCIA-TELLI P., CAMPUSANO, V.
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 CODE 2009
- AUTH CONNER W.C., ALKON P. U.
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- AUTH CUMMINS D.M., ROSTER D.F.
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- AUTH CUMMINS T.J.
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- AUTH COOK P.D., BESTLAKI D.W.
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- AUTH COOK P.D., BESTLAKI C.
TITL MICROBIOLOGICAL DEGRADATION OF NORTHERN CANADIAN OILS
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- AUTH COOK G.S.
TITL NON-TIDAL CIRCULATION IN AN OIL DRIFT BOTTLE AND
SEA BED DRIFTER EXPERIMENTS (1962-1963)
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ABST THE FEATURES OF THE DRIFT PATTERNS ARE DISCUSSED
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METEOROLOGICAL EFFECTS.
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- AUTH COOK R.V.
TITL OIL TRANSPORTATION BY SEA
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ABST THIS IS GULF OIL'S APPROACH TO SUPERMARRS AND
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KEYS SUPERMARRS, TERMINALS, TRANSPORTATION
CODE 3037A
- AUTH COOPER B.S.
TITL LAND DERIVED POLLUTANT HYDROCARBON
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- AUTH COOPER E.S., PERRE E.P.
TITL A THREE-DIMENSIONAL NUMERICAL MODEL TO CALCULATE
CURRENTS IN COASTAL WATERS UTILIZING A DEPTH
VARYING VERTICAL EDDY VISCOSITY
PUBL MASSACHUSETTS INSTITUTE OF TECHNOLOGY RALPH W.
PARSONS LABORATORY
ABST A 3-D NUMERICAL MODEL IS PRESENTED WHICH IS
SIMILAR TO 3-D GALERKIN MODELS RECENTLY DEVELOPED
BY VARIOUS INVESTIGATORS. THESE PREVIOUS MODELS
REQUIRE REASONABLE COMPUTER TIME AND STORAGE
REQUIREMENTS, AN ADVANTAGE NOT SHARED BY 2-D
MODELS BASED ON OTHER NUMERICAL SCHEMES.
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MODEL
CODE 7719 F
- AUTH COOPER R.A.
TITL DEEPWATER PORTS: HOW DO WE GET THERE FROM HERE?
PUBL UNKNOWN
ABST THIS PAPER DISCUSSES THE CONCERN FOR DEEPWATER
PORTS.
KEYS DEEPWATER PORTS, TRADE PATTERNS, INSTITUTIONS
CODE 7160F
- AUTH CORNACK G., NICHOLS J.A.
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CROWN COPYRIGHT 1977, ISBN 0 8524 107 5, 14
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ASSESS THE FEASIBILITY OF APPLYING DISPERSANT
CONCENTRATES FROM AIRCRAFT TO DISPERSE OIL SPILLS
AT SEA
KEYS DISPERSANTS, AIRCRAFT, TECHNIQUES, OPERATIONAL
FACTORS
CODE 7194F
- AUTH CORNACK G., JEFFERY P.C.
TITL AN OIL POLLUTION CONTROL OFFICER TRAINING COURSE
PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL
POLLUTION
ABST TOPICS INCLUDED IN THIS REPORT ARE OF NATURE AND
SOURCE OF OIL SPILLS; BEACH PROTECTION AND
CLEANUP AND THE RECOVERY OF OIL FROM WATER
SURFACES.
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- AUTH CORNACK G., NICHOLS J.A.
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FROM NATURAL AND CHEMICAL INDUCED DISPERSION OF
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PUBL 1977 OIL SPILL CONFERENCE
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DISPERSION INTO THE WATER COLUMN.
KEYS DISSIPATION, EMULSION, FORMATION, SPREADING
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- AUTH CORNACK G., NICHOLS J.A.
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PROBLEMS OF OIL SPILL CLEARANCE
PUBL WARREN SPRING LABORATORY
- ABST THIS PAPER DESCRIBES, BY WAY OF INTRODUCTION ONLY,
THE U.K. RESPONSE CAPABILITY FOR OIL SPILL
CLEARANCE AND OUTLINES THE REASONS FOR EMULSION A
DISPERSANT APPROACH. THE PAPER THEN CONCENTRATES
ON THE DETAILS OF THE SYSTEM USED TO REACH THE
DISPERSANT APPROACH OPERATIONAL
KEYS DISPERSANTS, SPREADING, AGITATION, TOXICITY
CODE 7134F
- AUTH CONNOR E.C.S., SOUTHWARD R.J., SOUTHWARD E.C.
TITL TOXICITY OF OIL SPILL WRECKERS TO MARINE LIFE: AN
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INDELICUS
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- AUTH CONNELL P., SPAULDING H., REEV R.
TITL THE PHYSICAL BEHAVIOUR OF OIL IN THE MARINE
ENVIRONMENT
PUBL DEPT. OF LEARN ENGINEERING, UNIV. OF BRISTOL ISLAND
ABST THIS PAPER IS INTENDED AS AN ASSESSMENT OF THE
PRESENT STATUS OF OIL SPILL MODELING. THE FIRST
SECTION IS DEVOTED TO AN OVERVIEW OF OIL SPILL
MODELS RELATIVE TO THEIR INTENDED APPLICATIONS.
THIS IS FOLLOWED BY A DESCRIPTION OF THE OIL OIL
SPILL FISHNETS INTERACTION MODEL AND ITS
APPLICATION TO A SIMULATED OIL SPILL. AN OIL SPILL
AN EVALUATION OF THE STATE OF KNOWLEDGE REGARDING
FUNDAMENTAL OIL SPILL PROCESSES & THE RELATIVE
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- AUTH COUSINS J.C.
TITL VAPOR-LIQUID EQUILIBRIUM OF HYDROCARBONS IN
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- AUTH COWELL E.B.
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ABST THIS BOOK STUDIES THE EFFECT OF OIL POLLUTION ON
SALT MARSHES AND ECOLOGICAL EFFECTS ON SHORT
COMMUNITIES. THERE ARE MANY STATISTICS, BUT THEY
DEAL MAINLY WITH BIOLOGICAL CONSIDERATIONS AND ARE
SOMEWHAT OUTDATED.
CODE 3086F
- AUTH COWELL E.B., COE G.V., DUMMIT W.R.
TITL APPLICATION OF ECOSYSTEM ANALYSIS TO OIL SPILL
IMPACT
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ABST ECOLOGICAL PRINCIPLES IN SELECTION OF OIL SPILL
CLEAN-UP DEVICES, SETTING CLEAN-UP PRIORITIES AND
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THEIR PROPER APPLICATION TO MINIMIZE ECOLOGICAL
DAMAGE AND TO PROPERLY EVALUATE THAT DAMAGE.
OIL SPILL, CLEAN-UP, ECOSYSTEM
CODE 7755F
- AUTH COX B.A., ANDERSON J., PARKER J.C.
TITL AN EXPERIMENTAL OIL SPILL: THE DISTRIBUTION OF
AROMATIC HYDROCARBONS IN THE WATER, SEDIMENT AND
ANIMAL TISSUES WITHIN A SWAMP POND
PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL
POLLUTION
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SEDIMENTS, AND TISSUES OF MARINE ORGANISMS AFTER
THE SPILL. DATA COMPILED IN THIS STUDY WERE
COMPARED TO FINDINGS OF VARIOUS FIELD AND
LABORATORY INVESTIGATIONS.
LABORATORY INVESTIGATIONS,
DIESEL FUEL, MORTALITIES, SEDIMENTS
CODE 0504F
- AUTH CRAIG G.D.
TITL A WAVE-INTERACTION MODEL FOR THE GENERATION OF
WINDROWS
PUBL J. FLUID MECHANICS, VOL. 41, PART 4, 1973
ABST INTERACTIONS OF SUITABLE PAIRS OF GRAVITY WAVES IN
A SHEAR FLOW ARE FOUND TO GIVE USE TO A PERIODIC
OR NEARLY PERIODIC SECONDARY MOTION.
KEYS GRAVITY WAVES, LANGMUIR VORTICES, WINDROWS
CODE 6312F
- AUTH CRAPP G.B.
TITL THE BIOLOGICAL EFFECTS OF RASING OIL POLLUTION AND
SHORE CLEANING
PUBL FIELD STUDIES COUNCIL OIL POLLUTION RESEARCH UNIT
ANNUAL REPORT 1969
CODE 5005F
- AUTH CRETNEY H.J., MONE G.S., GREEN D.R., BAUDEN C.A.
TITL LONG TERM FATE OF A HEAVY FUEL OIL IN A SPILL
CONTAMINATED B.C. COASTAL BAY
PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
ABST ON JAN. 24, 1973, THE FREIGHTER IRIS STARDUST RAN
AGROUND BETWEEN THE NORTHERN END OF VANCOUVER
ISLAND AND THE NARROWS OF BRITISH COLUMBIA CA

- MADRIDINON BEEF IN BONGOSIUM STRAIT. THE ACCIDENT
CAUSE THE RELEASE OF ABOUT 200 TONS OF 1000
SECOND FUEL OIL. THIS REPORT DOCUMENTS THE PATH OF
THE OIL STRANDED THERE.
KEYS
CODE 2600F
- AUTH CROCKER A.D., CRUMSHAW J.
TITLE THE EFFECT OF A CRUDE OIL ON INTESTINAL ABSORPTION
IN MUCKLINGS
PUBL ENVIRONMENTAL POLLUTION JOURNAL, NOV. 1974
ABST THIS PAPER DISCUSSES TEST RESULTS OF CRUDE OIL IN
DUCKS.
KEYS
CODE 2123 F
- AUTH CROSS R., ROBERTS A., CUMMINGHAM J., BATT G.
TITLE OIL SPILL CONTROL MANUAL FOR FIRE DEPARTMENTS
PUBL US EPA, TECHNOLOGY SERIES EPA-62-78-117 FEB. 1973
CODE 0400A
- AUTH CROSS R.
TITLE SMALL VACUUM OIL SKIMMING SYSTEM
PUBL PROJECT ISOBUFF, PRO. 1973
CODE 0035A
- AUTH CROSS R., CUMMINGHAM J.J.
TITLE OIL BOOMS FOR EMERGENCY MARINA USE
PUBL JOURNAL OF WATERWAYS, HARBORS AND COASTAL EGR
DIVISION, ASCE, VOL. 99, NO. 1, 1973
CODE 0729R
- AUTH CROSS R., MOULT D.P.
TITLE COLLECTION OF OIL SLICKS
PUBL ASCE NATIONAL MEETING ON TRANSPORTATION
ENGINEERING, JULY 13-17, 1970
ABST MATHEMATICAL DERIVATIONS AND CALCULATIONS ARE USED
TO DESCRIBE THE EFFECTIVENESS OF OIL SLICK
SKIMMERS.
CODE 3047-
- AUTH CROSS R., MOULT D.P.
TITLE OIL BOOMS IN TIDAL CURRENTS
PUBL JOURNAL OF WATERWAYS, HARBORS, AND COASTAL EGR.
DIVISION, ASCE, VOL. 99, NO. 1, 1973
CODE 0730R
- AUTH CROSWELL W.F., PARKER A.W., BOPIA L.P.
TITLE REPORT OF JAN. 21 - FEB. 1, 1970 MEETING, AD HOC
COMMITTEE ON SPACE MONITORING OF OIL SPILLS
PUBL LAMLEY RESEARCH CENTER, JUNE 16, 1970
ABST MEETING WAS CONVENED TO DISCUSS USER REQUIREMENTS,
CURRENT INVESTIGATIONS AND CAPABILITIES, FUTURE
PLANS AND PROBLEM AREAS ATTENDANT TO OIL SPILL
DETECTION AND CONTROL. THE RESULTS OF THE MEETING
ARE CONTAINED IN THIS REPORT.
KEYS
CODE 7691F
- AUTH CROWLEY W.
TITLE ARMY NAVYSHIP 0004-000-1010
PUBL DEPT. OF THE NAVY, NAVAL SHIP SYSTEMS COMMAND
ABST THE RECOVERY OF BUNKER C FUEL OIL FROM THE SUNKEN
TANKER SS ARROW AND CONCURRENT MEASURES ARE
DISCUSSED.
KEYS
CODE 0331F
- AUTH CRUMP-WIESNER M.J., JENNINGS A.L.
TITLE PROPERTIES AND EFFECTS OF NON-PETROLEUM OILS
EPA FOR EPA 1975 CONFERENCE
PUBL DEALS WITH SPILLS OF NON-PETROLEUM OIL IN AN
AQUATIC ENVIRONMENT APPROX. 9 PERCENT OF SPILLS
ARE NON-PETROLEUM BUT LITTLE OR NO WORK HAS BEEN
DONE WITH THEM.
KEYS
CODE 0073R
- AUTH CSZNAUD G.T.
TITLE TURBULENT DIFFUSION IN THE ENVIRONMENT
PUBL GEOPHYSICS AND ASTROPHYSICS
ABST AVAILABLE AT UMI LIBRARY
KEYS
CODE 0500F
- AUTH CUNDELL B.W., TRABLER R.W.
TITLE HYDROCARBON-DEGRADING BACTERIA ASSOCIATED WITH
ARCTIC OIL SPILLS
PUBL DEPT. OF PLANT PATHOLOGY-ENTOMOLOGY, UMI FOR
AMERICAN INSTITUTE OF BIOLOGICAL SCIENCES, 1974
ABST 15 HYDROCARBON-DEGRADING BACTERIA WERE ISOLATED BY
ENRICHMENT CULTURE FROM AN AGED ASPHALTIC PICO ALASKA
A NATURAL OIL SEEP, CAPE SIMPSON ALASKA. THE
ENRICHMENT SUBSTRATES WERE NO. 1 AND NO. 6 FUEL
OILS AND NAPHTHALENE. THE BACTERIA WHICH
REPRESENTS A RANGE OF GENERAL GRAM AT THE EXPENSE
OF ALIPHATIC AROMATIC AND NAPHTHALENE
HYDROCARBONS. THE GROWTH TEMP. OF THE ORGANISMS
SUGGEST THAT THE ISOLATES WERE FACULTATIVE
PSYCHROPHILIC BACTERIA.
CODE 0122R
- AUTH CUMMINGHAM C.B., EYON J., CRUM J.S.
TITLE THE DESIGN OF AN EFFECTIVE POLLUTION CONTAINMENT
BARRIER FOR THE OPEN SEA
PUBL OCEANOGRAPHIC TECHNOLOGY CONFERENCE, PAPER NO. 0410.
- MAY 1-3, 1972
ABST THIS PAPER DESCRIBES THE DEVELOPMENT AND TESTING
OF THE BOTTOM TENSION BOOM
KEYS
CODE 0303F
- AUTH CUMMINGHAM J.J.
TITLE A RAPIDLY DEPLOYABLE OIL CONTAINMENT BOOM FOR
EMERGENCY MARINA USE
PUBL GOVERNMENT REPORTS ANNOUNCEMENTS
CODE 0310R
- AUTH CUTLER W.C., DAVIS R.C.
TITLE DETERGENT THEORY AND TEST METHODS. PART I
PUBL MARCEL DEKLER INC., SURFACTANT SCIENCE SERIES,
VOL. 5, 1972
ABST THIS VOLUME, IN 2 PARTS, PRESENTS A COMPILATION OF
TEST METHODS IN USE TODAY, AS WELL AS A THOROUGH
EXAMINATION OF THE THEORETICAL BASIS OF THESE
TESTS.
KEYS
CODE 7008E
- AUTH CWIN A.
TITLE FEDERAL RESEARCH AND DEVELOPMENT PROGRAM FOR OIL
SPILLS
PUBL UNKNOWN
ABST DISCUSSES RESEARCH AND DEVELOPMENT PROGRAMS FOR
PREVENTING OIL SPILLS.
KEYS
CODE 0804F
- AUTH DAILEY J.J., CASSIDY P.E., YAGER B.J.
TITLE BEACH PROTECTION BY A DEGRADABLE, SPRAYED FILM
PUBL TRALUA INC., FOR EPA 1975 CONFERENCE
ABST THE BEST RESULTS OF BEACH PROTECTION AGAINST
OIL-SPILLED OIL SPILLS BY MEANS OF A SPREADABLE
POLYMER IS UNDER LAB CONDITIONS. FILM IS QUITE
EASY TO DEGRADE.
KEYS
CODE 0120R
- AUTH DAVIES J.T., DRISCOLL P.
TITLE EDDIES AT FREE SURFACES, SIMULATED BY PULSES OF
WATER
PUBL IND. ENG. CHEMICAL FUNDAMENTALS, VOL. 13, NO. 2,
1974
ABST STUDIES OF PULSES IN WATER COLORED WITH
PHENANTHRALENE AND PHOTOGRAPHED AS THEY ARE
PROJECTED UPWARD TOWARD A HORIZONTAL FREE SURFACE.
KEYS
CODE 0310F
- AUTH DAVIS C.E., RAC A.E., SEANASSIS J.J., MOUSSA M.L.
TITLE MULTILEVEL TANK BOLLING POINT GAS CHROMATOGRAPH
FOR MONITORING OIL POLLUTION
PUBL OIL SPILL DEVELOPMENT LG. FOR EPA 1975 CONFERENCE
KEYS
CODE 0080F
- AUTH DEAN R.C.
TITLE DEVELOPMENT OF A MOBILE SYSTEM FOR CLEANING OIL
CONTAMINATED BEACHES
PUBL EPA, REPORT-62-73-233
CODE 0404R
- AUTH DEDEA D.
TITLE THE DISASTERS THAT DIDN'T
PUBL ERSA, USA THIRD QUARTER, 1977
ABST THIS REPORT DISCUSSES THE EFFECTS OF A SPILL ON
THE ENVIRONMENT.
KEYS
CODE 1226F
- AUTH DELACOUR J., DENYSER J.
TITLE PERFORATING USED FOR DEEP-WATER SEABED
RECONNAISSANCE
PUBL OCEAN INDUSTRY, VOL. 5, NO. 7, JULY 1970
ABST ARTICLE DEALS WITH A LOW-COST PERFORATING METHOD
WHICH PERMITS EASY TRIPPING AND COMPLETE BEHIND
CONTROL OF DRILLING AND CURING.
CODE 3042R
- AUTH DENNINGTON V.M., GEORGE J.J., WYBORN C.M.L.
TITLE THE EFFECTS OF OILS ON GROWTH OF FRESHWATER
PHYTOPLANKTON
PUBL ENVIRONMENTAL POLLUTION VOL. 8, NO. 3, APRIL 1973
ABST IN VIEW OF THE ECOLOGICAL SIGNIFICANCE OF
FRESHWATER PHYTOPLANKTON AS PRIMARY PRODUCERS IN
THE AQUATIC ENVIRONMENT, SURPRISINGLY LITTLE IS

- ENOUGH OF THEIR TOLERANCE TO OIL POLLUTION.
 CODE 3046
- AUTH DENNIS D.
 TITLE EFFECTIVELY RECOVERING OIL SPILLS TO GROUNDWATER
 PUBL UNKNOWN
 ABST THIS ARTICLE REVIEWS THREE METHODS FOR RECOVERY OF GROUNDWATER OIL SPILLS.
 REYS RECOVERY WELLS, RECOVERY TRENCH, CRACK RECOVERY SYSTEM
 CODE 6056F
- AUTH DENNIS J.W.
 TITLE OIL POLLUTION SURVEY OF THE U.S. ATLANTIC COAST
 PUBL API, DIVISION OF TRANSPORTATION, MAY 15, 1959
 ABST SPECIAL REFERENCE IS MADE TO THE SOUTHEAST FLORIDA COAST CONDITIONS AT THIS TIME.
 REYS SURVEY, ATLANTIC COAST, SOUTHEAST FLORIDA COAST
 CODE 0041H
- AUTH DENNIS J.W.
 TITLE UNITED STATES COAST GUARD HIGH SEAS OIL CONTAINMENT SYSTEM (MOSCOT)
 PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
 ABST A DETAILED TECHNICAL DESCRIPTION OF THE HIGH SEAS OIL CONTAINMENT SYSTEM IS PRESENTED.
 REYS CONTAINMENT, BARRIERS, MARKINGS, HANDLING, STRATEGIC EQUIPMENT
 CODE 0524F
- AUTH UER J.W. BRUNNEN D.
 TITLE AN OFFSHORE MECHANIZED SOBBENT OIL RECOVERY SYSTEM USING VESSELS OF OPPORTUNITY
 PUBL CIVIL ENGINEERING LAB., NAVAL CONSTRUCTION BATTALION CENTER, PDAI NUMBER, G.A. REPORT AC. N-1476 34-DEC, MARCH 1977
 ABST THE UNIQUE FEATURE OF THIS CONCEPT IS THE WAVE PULLING CHARACTERISTICS OF THE SEAM CHIPS WHICH SERVE TO SURE THE OIL FROM THE WATER
 REYS RECOVERY, ABSORBERS, SOBBENTS
 CODE 0876F
- AUTH DER J.J., SMOAKLEY E.
 TITLE OIL CONTAMINATED BEACH CLEANUP
 PUBL CIVIL ENGINEERING LAB., 69-110, NAVAL UNDERSEAS SYSTEMS CENTER, NAVAL SHIP SYSTEMS COMMAND, N-1337, APR, 1974
 ABST THE MOST EFFECTIVE BEACH CLEANUP PROCEDURES AND EQUIPMENT HAVE BEEN IDENTIFIED AND TABULATED IN TERMS OF SELECTED BEACH CLASSIFICATION.
 REYS ENVIRONMENTAL RESTORATION, OIL CONTAINMENT SYSTEMS, RECOVERY, CLEANUP
 CODE 2410F
- AUTH DER J.J., LAMAR D.J.
 TITLE QUANTITATIVE EVALUATION OF MECHANICAL OIL SPILL CLEANUP DEVICES
 PUBL APPLIED CONTROL TECHNOLOGY
 ABST A SYSTEMATIC QUANTITATIVE METHOD HAS BEEN DEVELOPED WHICH CAN BE USED FOR PRELIMINARY SCREENING, FINAL EVALUATION AND SELECTION OF CANDIDATE OIL REMOVAL DEVICES.
 REYS RECOVERY, COST STUDIES, RECOVERY EQUIPMENT
 CODE 0615F
- AUTH DESHMAN G.
 TITLE STUDIES ON THE POLLUTION OF FISH MEAT BY MINERAL OILS. II. INJURY AND POLLUTION BROUGHT FORTH IN FISH BY OIL DISPERSIONS.
 PUBL BULL. JAP. OCCUP. ENV. FISH. 37:302-306, 1971
 CODE 10364H
- AUTH DEVANNY J.W.
 TITLE KEY ISSUES IN OFFSHORE OIL
 PUBL SECOND ANNUAL SEA GRANT LECTURE AND SYMPOSIUM
 CODE 0321A
- AUTH DEVANNY J.W.
 TITLE SURFACE FRACTIONATION AND VERTICAL DISPERSION OF OIL SLICKS
 PUBL PROPOSAL TO NATIONAL OCEANIC AND ATMOSPHERIC ADMINISTRATION, MARCH 1974
 CODE 2061H
- AUTH DEVANNY J.W., SIMPSON M., WEISLER T.
 TITLE THE HIT SINGLE SPECIES FISHERY SIMULATOR: APPLICATION TO THE GEORGES BANK YELLOWTAIL HIT SEA GRANT PAUGHAN REPORT NO. RITSU-77-21 DEC. 1977
 ABST THIS STUDY HAS TWO SETS OF GOALS: 1. THE DEVELOPMENT AND DOCUMENTATION OF A FISHERIES SIMULATOR AND 2. THE APPLICATION OF THIS MODEL TO THE GEORGES BANK YELLOWTAIL FISHERY.
 REYS FISHERIES SIMULATOR, STOCK-RECRUITMENT FEEDBACK SYSTEM, GEORGES BANK YELLOWTAIL FISHERY
 CODE 2084F
- AUTH DEVANNY J.W., STEWART R.J.
 TITLE ANALYSIS OF OIL SPILL STATISTICS
 PUBL PRIMARY PHYSICAL IMPACTS OF OFFSHORE PETROLEUM DEVELOPMENTS, III
 ABST ESTIMATES BY STATISTICAL ANALYSIS ARE GENERATED OF THE PROBABILITIES OF SPILLAGE BY THE NUMBER AND SIZE OF INDIVIDUAL SPILLS.
 CODE 3110H
- AUTH DEWITT F.A., MELVIN P.
 TITLE OIL SPILL AND OIL POLLUTION REPORT, NOV. 1974 - FEB. 1975, FEB. 1975 - APRIL 1975, JULY 1975 - OCT. 1975
 PUBL MARINE SCIENCE INSTITUTE, UNIVERSITY OF CALIF., NO. 88336J
 ABST SUMMARIES AND BIBLIOGRAPHIC LITERATURE CITATIONS COMMENT STATUS OF SOME OF THE RESEARCH PROJECTS AS LISTED IN REPORTS I AND II.
 REYS DETECTION, CONTROL, PREVENTION
 CODE 0050
- AUTH DH A.
 TITLE GRAIN SIZE CURVES ASSOCIATED WITH MARINE SLOPMENT IN THE VICINITY OF QUONSET POINT, RI.
 ABST STATISTICS ON OILS RUN THROUGH SIEVES - NO PAPER OR CONCLUSION INCLUDED
 CODE 3045F
- AUTH DICK J., FELDMAN B.
 TITLE EFFICIENCY AND RETENTIVITY TESTING AND PERFORMANCE OF SIMULANT AGENTS IN THE REMOVAL OF OIL SPILLS
 PUBL CONFERENCE ON SPILL TECHNOLOGY, EPC REPORT NO. SPS-3-11-73-11 APRIL 1973
 ABST THIS CONDENSED REPORT CONTAINS TECHNIQUES FOR THE TESTING OF SIMULANT AGENTS TO DETERMINE THEIR EFFICIENCY IN THE REMOVAL OF OIL AND THEIR ABILITY TO REMAIN UNOIL REMOVED BY THE ACTION OF SIMULANT.
 REYS REMOVAL, SIMULANT AGENT, OIL LAYER THICKNESS
 CODE 7152F
- AUTH DICKY T.B., LULARITZ R.T.
 TITLE US COAST GUARD REGULATION AND INCO RECOMMENDATIONS FOR LOW TANKERS
 PUBL USCG
 CODE 6504H
- AUTH DICKS B.
 TITLE SOME EFFECTS OF RUSSIAN CRUDE OIL ON THE LIMPET PATELLA VULGATA
 PUBL ENVIRONMENTAL POLLUTION, 9:131-134-225
 CODE 1052H
- AUTH DIEDERIKSEN J., HALL A.P.
 TITLE THE BURNING OF OIL IN WRECKED TANKERS: LARGE SCALE BURNING TEST
 PUBL ROCKET PROPULSION ESTABLISHMENT REPORT, DEC. 1972
 ABST EXPERIMENTS WERE CONDUCTED ON 175 TONS OF OIL TO DETERMINE BURNING CHARACTERISTICS.
 CODE 6040F
- AUTH DIEDERIKSEN J., HALL A.P., WINDL P.T.
 TITLE IGNITION AND COMBUSTION IN IN-SITU OIL FUEL WRECKED OIL TANKERS SMALL SCALE BURNING TESTS CARRIED OUT AT THE RPE
 PUBL ROCKET PROPULSION ESTABLISHMENT, AD 784906, JULY 1972
 ABST THE EFFECT OF THE SIZE AND POSITION OF VENTING APERTURES ON THE BURNING RATE OF CRUDE OIL IN WRECK TANKS HAS BEEN DETERMINED. ONE SIZE APERTURE AND ONE LID APERTURE IN ALL TESTS.
 CODE 6107H
- AUTH DILLON G.A., TINGLE A.C.
 TITLE A NUMERICAL STUDY OF RESCALABLE TRANSPORT OF AIR POLLUTANTS IN SEA-WALLZE CIRCULATIONS
 PUBL UNKNOWN
 ABST IN THIS STUDY A NUMERICAL MODEL IS USED TO EXAMINE THE DEVELOPMENT OF RESCALABLE AIRBORNE POLLUTANT DISTRIBUTIONS.
 REYS POLLUTANT DISTRIBUTIONS, SEA-WALLZE CIRCULATIONS, LAKE/SEA BREEZE PLEAS
 CODE 3230F
- AUTH DIETZ D.W.
 TITLE BEHAVIOR OF COMPONENTS FROM SPILLED OIL ON THEIR WAY THROUGH THE SOIL
 PUBL JOURNAL OF PETROLEUM TECHNOLOGY, 25:1045-1046
 CODE 1053F
- AUTH DIETZ R.S., LAFON E.
 TITLE NATURAL SLICKS ON THE OCEAN
 PUBL JOURNAL OF MARINE RESEARCH, 18:2, 1960
 ABST THIS PAPER SUMMARIZES A FEW OBSERVATIONS CONCERNING THE DISTRIBUTION AND ORIGIN OF NATURAL SLICKS.
 REYS NATURAL SLICKS, DISTRIBUTION, ORIGIN
 CODE 2053F
- AUTH DISALVO L.M., GAVIL M.E.
 TITLE HYDROCARBONS ASSOCIATED WITH SUSPENDED PARTICULATE MATTER IN SAN FRANCISCO BAY BAYEAS
 PUBL NAVAL BIOMEDICAL RESEARCH LAB., PDA EPA 1975 CONFERENCE
 REYS HYDROCARBONS, SUSPENDED PARTICULATE MATTER, SAN FRANCISCO BAY
 CODE 0080H
- AUTH DOE, ROBERT C., MARSH W.M., BELLS P.G.
 TITLE A SELECTED BIBLIOGRAPHY ON OIL SPILL DISPERSANTS
 PUBL ENVIRONMENTAL PROTECTION AGENCY ATLANTIC, FISHERIES AND ENVIRONMENT CANADA
 ABST A SELECTED AND INDEXED BIBLIOGRAPHY ON THE CHEMISTRY, BIOLOGICAL EFFECTS, USE AND

EFFECTIVENESS OF OIL SPILL DISPERSANTS IS PRESENTED. IT CONTAINS 304 REFERENCES, COMPILED ALPHABETICALLY AND INDEXED BY SUBJECT AND RETRIEVAL TO ALLOW RAPID ACCESS.

KEY: BIOGEOGRAPHY, DISPERSANTS, DISPENSING, OIL POLLUTION, SURFACTANTS, TOXICOLOGY, WATER POLLUTION.

CODE: 7735 F

AUTH: DOLAN F.A., BOMERSUJ, J.P.
 TITLE: DEVELOPMENT OF MOBILE SYSTEM FOR CLEANING OIL CONTAMINATED BEACHES.
 PUBL: PROJECT NO. 190001L
 ABST: THE SYSTEM INVOLVES WASHING OF THE SAND IN A HIGH ENERGY JET-CONTAINED WASHER AND SEPARATION OF THE CLEANED SAND FROM THE WASHING FLUID IN A CONCENTRIC SOLID-LIQUID CYCLONE.
 CODE: 6089K

AUTH: MARLEN J.S.
 TITLE: LIMITED OIL SPILLS IN MARSH AREAS
 PUBL: UNKNOWN
 ABST: THIS PAPER INVESTIGATES THE ACTUAL PROBLEMS WHICH CONTRIBUTE TO THE HIGH COST OF CLEANING UP AFTER AN OIL SPILL.
 KEY: CLEAN UP, REMOVAL, PROBLEMS
 CODE: 0518F

AUTH: MARLEN J.S., ATYAS A.J., MOUTER D.
 TITLE: HIGH CURRENT CONTROL OF FLUATING OIL
 PUBL: CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
 ABST: THIS PAPER DISCUSSES THE DESIGN, DEVELOPMENT AND DEMONSTRATION OF A STREAMLINED BULK UTILIZATION HYDRAULIC CLEANUP.
 KEY: BARRIERS, CONTAINMENT
 CODE: 0543F

AUTH: DOWNS J.P.
 TITLE: CONTROL OF OIL SPILLAGE BY DUMPS
 PUBL: US CURS OF OIL, DIPL. OF THE ARMY, 1967
 CODE: 0722F

AUTH: DONWELL R.B., WILSON R.P., CHEN Y.L., TEYSANJIL E.
 TITLE: FINAL REPORT, OFFICE METER RESEARCH, THEORETICAL STUDY OF FLOW THROUGH CONCENTRIC ORIFICES
 PUBL: PIPELINE RESEARCH COMMITTEE FOR AMERICA AND ASSOCIATION, PH-80-50, SEPT. 1, 1972
 ABST: THE OBJECTIVE OF THE PROJECT WAS TO CREATE A THEORETICAL MODEL OF THE FLOW THROUGH ORIFICES WITH THE ULTIMATE GOAL OF IMPROVING THE MEASUREMENT ACCURACY OF GAS FLOW WHEN USING ORIFICES.
 KEY: FLOW PATTERNS, DISCHARGE COEFFICIENTS, CONCENTRIC ORIFICES
 CODE: 6036E

AUTH: BRAGGON M., COLLEY M.J.
 TITLE: OIL CONTAINMENT WITH
 PUBL: MARINE CURP, FDA EPA NO. 68-03-0205, SSIE NO. 08A-1022
 CODE: 0664F

AUTH: DRARE R.
 TITLE: ENERGY TECHNOLOGY FOR SELF-SUFFICIENT
 PUBL: CONSTRUCTION ENGINEERING, INC.
 CODE: 2941K

AUTH: DRARER A.A.
 TITLE: A DIFFUSION-DEPOSITION SCHEME FOR USE WITHIN THE AIR TRAJECTORY MODEL
 PUBL: AIR RESOURCES LABORATORIES, DEC. 1970
 ABST: A FINITE DIFFERENCE METHOD FOR VERTICAL DIFFUSION AND DEPOSITION HAS BEEN DEVELOPED AND INCORPORATED INTO THE EXISTING AIR TRAJECTORY MODEL. THE FINITE DIFFERENCE MULTI-BOX MODEL PERMITS TEMPORAL VARIATIONS OF VERTICAL DIFFUSIVITY PROFILES AND DEPOSITION PARAMETERS. THE MULTI-BOX IS PRESENTED INCLUDING SOME EXAMPLES OF ITS APPLICATION TO LAGRANGIAN TRAJECTORIES WITH RESPECT TO OY DEPOSITION AND DIURNAL STABILITY CHANGES.
 KEY: FINITE DIFFERENCE METHOD, VERTICAL DIFFUSION, AIR TRAJECTORY
 CODE: 6050F

AUTH: DUBOVIK A.S.
 TITLE: PHOTOGRAPHIC RECORDING OF HIGH SPEED PROCESSES
 PUBL: CLEANINGHOUSE FOR FEDERAL SCIENTIFIC & TECHNICAL INFORMATION
 ABST: DESCRIBES METHODS OF THE PHOTOGRAPHIC RECORDING OF HIGH SPEED PROCESSES AS WELL AS HIGH SPEED PHOTOGRAPHIC APPARATUS. THESE METHODS ARE PRESENTLY USED IN THE STUDY OF MANY NEW AREAS OF PHYSICS & TECHNOLOGY. THIS MONOGRAPH IS CONCERNED WITH ALL THE BASIC PROBLEMS OF THE PHOTOGRAPHIC RECORDING OF HIGH SPEED PROCESSES: THE THEORY & METHODS OF THE CONSTRUCTION OF APPARATUS; THE SELECTION OF AN APPARATUS FOR THE SOLUTION OF A GIVEN PROBLEM; SPECIAL METHODS OF STUDYING THE PHYSICAL PARAMETERS OF HIGH SPEED PROCESSES, ETC.
 KEY: OPTICAL SYSTEMS, OPERATING PRINCIPLES, PROPAGATION OF SHOCK WAVES
 CODE: 7001F

AUTH: BRUCE R.A.

TITLE: ATMOSPHERIC POLLUTANT TRANSPORT AND DEPOSITION ON THE SEA SURFACE
 PUBL: URI, SCHOOL OF OCEANOGRAPHY
 CODE: 0337K

AUTH: DULL R.A., QUINN J.W., LONEY C.E.
 TITLE: ENFOLDMENT OF HEAVY METALS AND ORGANIC COMPOUNDS IN THE SURFACE MICROLAYER OF MARGANSETTI BAY, RI
 PUBL: SCIENCE 176
 CODE: 0338K

AUTH: DUDLEY G.
 TITLE: THE INCIDENCE AND TREATMENT OF OIL POLLUTION IN OIL PORTS
 PUBL: UNKNOWN
 ABST: SUMMARY AND UPDATE OF PREVIOUS PAPERS PRESENTED BY THE AUTHOR ON THE SUBJECT OF INCIDENTAL AND TREATMENT OF OIL POLLUTION IN OIL PORTS.
 KEY: TERMINALS, TANKERS, OIL PUMPS
 CODE: 7161F

AUTH: DUDLEY G., MAYIF R.P.
 TITLE: MANY VARIABLES GO INTO PLANNING DEEPWATER TERMINAL
 PUBL: OIL AND GAS JOURNAL
 CODE: 0478K

AUTH: DURDEN P.C.
 TITLE: SPILL IN PORTUGAL A REPORT OF THE JARAC MAERSK INCIDENT
 PUBL: ENVIRONMENTAL EMERGENCY BRANCH EPS CANADA, REPORT NO. EPS-80-11-70-1, SEPT. 1975
 ABST: THIS REPORT DEALS WITH THE SPILL OF OIL FROM THE DANISH TANKER, JARAC MAERSK WHICH GROUNDWRECK ON THE COAST OF NORTHERN PORTUGAL IN LATE JAN. 1975
 KEY: CLEANUP, BEHAVIOR AND EFFECTS OF OIL, TANKERS, JARAC MAERSK
 CODE: 7143F

AUTH: DUERK C.
 TITLE: HOW DID URI GET INVOLVED IN THIS MESS? URI ALUMNI BULLETIN, VOL. 4(1), NO. 8, SPRING 1977
 ABST: WHEN THE LIBERIAN TANKER ARGO RECHANT ELSTI RAN GIL TO THE SEA OFF NANTUAET ISLAND IN DEC., URI'S OCEAN SCIENTISTS WENT TO OCHA.
 KEY: ARGO RECHANT, ENVIRONMENTAL EMERGENCY, IMPACT
 CODE: 7066F

AUTH: DUKE R.W., CAVIS H.E., DENNIS A.J.
 TITLE: ENVIRONMENTAL ASSESSMENT BIOLOGICAL TESTS FOR PILOT STUDIES - EARL-RTP PROCEDURES MANUAL: LEVEL 1
 PUBL: EPA OFFICE OF RESEARCH AND DEVELOPMENT, EMER23, APRIL 1973, EPA 600/7-77-013
 ABST: THIS MANUAL GIVES LEVEL 1 BIOLOGICAL TESTING PROCEDURES FOR PERSONNEL EXPERIENCED IN COLLECTING, SUBSAMPLING OR SAMPLES FROM INDUSTRIAL AND ENERGY PRODUCING PROCESSES.
 KEY: BIOASSAY, SAMPLING, ANALYZING
 CODE: 7160F

AUTH: DUMBAR H.J.
 TITLE: STABILITY AND FRAGILITY IN ARCTIC ECOSYSTEMS
 PUBL: ARCTIC 26(1):177-185, 1973
 CODE: 1054K

AUTH: DUNN C.W., MALE L.Z. (COORDINATOR)
 TITLE: THE OAT BIR: ARCTIC ISLAND MARINE BIOGEOGRAPHY - REVISED EDITION VOLUMES 1 AND 2
 PUBL: URI COASTAL RESOURCES CENTER MARINE TECHNICAL REPORT 70, 1970, BIOGEOGRAPHY
 ABST: VOLUME 1 - SEA CROSS REFERENCED SECTIONS - DOCUMENT LISTING, AUTHOR INDEX, CORPORATE INDEX, GEOGRAPHICAL LISTING MAP LISTING, MARGANSETTI BAY SAMPLING STATIONS LISTING ON MARINE ENVIRONMENT OF RI AND NEARBY WATERS. VOLUME 2 - THE OAT BIR IS DESIGNED SO THAT ALL THE INFORMATION NECESSARY TO OBTAIN A COPY OF A PUBLICATION CAN BE QUICKLY AND EASILY FOUND WITH WHATEVER PART A RESEARCHER BELONGS.
 KEY: MARINE BIOGEOGRAPHY
 CODE: 7744K

AUTH: DUNN W.A., TULLIER P.W.
 TITLE: SPILL RISK ANALYSIS PROC. PHASE II METHODOLOGY DEVELOPMENT AND DEMONSTRATION
 PUBL: OPERATIONS RESEARCH, INC., USCG, AUG. 1974
 ABST: THIS REPORT DESCRIBES RESEARCH AND RESULTS IN THE DEVELOPMENT AND DEMONSTRATION OF SYSTEMATIC METHODS OF ASSESSING THE EFFECTIVENESS OF EXISTING PROPOSED OR RECENTLY IMPLEMENTED MARINE SAFETY REGULATIONS.
 CODE: 6106F

AUTH: DYE L.
 TITLE: BLOWOUT AT PLATFORM A
 PUBL: KNOWLEDGE AND CO., INC. 1971
 ABST: ANOTHER ANALYSIS OF THE SANTADAARA OIL SPILL.
 CODE: 3065K

AUTH: EARLES R.
 TITLE: STADY-STATE THEORY OF TOWING CABLES
 PUBL: QUARTERLY TRANSACTIONS OF THE ROYAL INSTITUTION OF NAVAL ARCHITECTS, APRIL 1960, VOL. 110, NO. 2
 ABST: THIS PAPER SETS A BASE FOR DEVELOPMENT OF A TOWING CABLE BY PRESENTING THE THEORY OF TOWING.
 KEY: HYDRODYNAMICS, TOWED BODY CHARACTERISTICS, CABLE

- CHARACTERISTICS
CODE 0806F
- AUTH EASTON R.
TITLE BLACK TIDE: THE SANTA BARBARA OIL SPILL AND ITS CONSEQUENCES
PUBL DELACOSTE PRESS, NEW YORK 1972
ABST THIS IS A COMPLETE REPORT ON THE SANTA BARBARA OIL SPILL WITH EMPHASIS ON THE REACTIONS OF THE CITIZENS OF SANTA BARBARA.
CODE 3081R
- AUTH EDDY, METCALF, INC.
TITLE WASTEWATER ENGINEERING AND MANAGEMENT PLAN FOR BOSTON HARBOUR-EASTERN MASSACHUSETTS METROPOLITAN AREA
PUBL EMRA STUDY-SUMMARY REPORT
ABST THIS REPORT SUMMARIZES RESULTS OF STUDY ON COMBATING POLLUTION IN THE EASTERN MASSACHUSETTS METROPOLITAN AREA.
KEYS WATER ORIENTED, LAND DISPOSAL, INDUSTRIAL WASTE
CODE 8522F
- AUTH EDGERTON A.T., REEKS D., WILLIAMS D.
TITLE MICROWAVE EMISSIONS CHARACTERISTICS OF OIL SLICKS
PUBL JOINT CONFERENCE ON SENSING OF ENVIRONMENTAL POLLUTANTS, NOV. 1971
CODE 0400K
- AUTH EDGERTON A.T., TRELLER D.T.
TITLE FINAL REPORT, RADIOMETRIC DETECTION OF OIL SLICKS
PUBL USCC, APPLIED TECHNOLOGY DIVISION, JAN. 1970, AL. SD1335-1
ABST A STUDY HAS BEEN PERFORMED TO ASSESS THE FEASIBILITY TO USE MICROWAVE RADIOMETRY FOR DETECTION OF OIL POLLUTION.
KEYS DETECTION, SURVEILLANCE, MICROWAVES, RADIOMETRY
CODE 2062F
- AUTH EDWARDS M.
TITLE ROLE OF THE FEDERAL GOVERNMENT IN CONTROLLING OIL POLLUTION AT SEA
PUBL OIL ON THE SEA, PLENUM PRESS, 1969
ABST THIS ARTICLE EXAMINES SOME OF THE PROBLEMS AND TRENDS BRIEFLY UPON EXISTING AUTHORITIES IN CONTROLLING OIL POLLUTION OF THE SEA. IT ALSO LOOKS AT PENDING CONGRESSIONAL ACTION.
CODE 3028H
- AUTH EIDON C., FITZPATRICK R., CONLON J.
TITLE THE CASCO BAY OIL SPILL: PROBLEMS OF CLEANUP AND DISPOSAL
PUBL EPA, REGION 1, DIVISION OF SURVEILLANCE AND ANALYSIS FOR 1975 CONFERENCE
ABST STUDY OF A LACK OF LOCALLY AVAILABLE EQUIPMENT LOGISTICS INVOLVED IN BUYING NEW AND EQUIPMENT IN NUMEROUS ISLANDS WHICH WERE AFFECTED BY THE SPILL, AND DISPOSAL OF LARGE AMOUNTS OF OIL SOAKED BOATS PRESENTING LOGICAL PROBLEMS TO DOMESTIC PERSONNEL.
KEYS CLEANUP, DISPOSAL, CASCO BAY, OIL SOAKED BOATS
CODE 0090F
- AUTH EISLER R.
TITLE SOME EFFECTS OF A SYNTHETIC DETERGENT ON THE ESTUARINE FISH
PUBL AMERICAN FISH SOCIETY, 04-70-31
CODE 1080K
- AUTH EISLER R.
TITLE TOXIC, SUBLETHAL AND LATENT EFFECTS OF PETROLEUM ON RED SEA MACROFAUNA
PUBL USEPA, NATIONAL MARINE WATER QUALITY LAB., BARRINGTONS, RI FOR EPA 1975 CONFERENCE
KEYS TOXICITY, SUBLETHAL AND LATENT EFFECTS, RED SEA MACROFAUNA
CODE 0145F
- AUTH ELDERING M.C.
TITLE OIL SPILL SURVEILLANCE SYSTEMS
PUBL EPA
CODE 0433F
- AUTH ENRIGHT R.J.
TITLE STEEL OR CONCRETE PLATFORMS FOR THE NORTH SEA - OR NEITHER?
PUBL THE OIL AND GAS JOURNAL, JUNE 30, 1975
ABST DISCUSSION OF THE PROS AND CONS OF STEEL VS. CONCRETE PLATFORM FOR OIL DRILLING.
KEYS PLATFORMS, NORTH SEA, CONCRETE, STEEL
CODE 5094F
- AUTH ENVIRONMENTAL RESOURCE LTD.
TITLE CLEANING AND CONDITIONING AGENTS: THEIR IMPACT ON THE ENVIRONMENT IN THE U.K.
PUBL GRAMM AND THOMAS LIMITED
ABST THIS REPORT EXAMINES THE QUANTITY OF CLEANING AND CONDITIONING PRODUCTS USED IN THE COMMUNITY AND THE NATURE OF THEIR CONSTITUENTS. IT REVIEWS THE EVIDENCE ON THE EFFECTS ON THE ENVIRONMENT OF THE FOLLOWING: SURFACTANTS, PHOSPHATES AND OTHER DETERGENT BUILDERS, BLEACHING AGENTS, FLUORESCENT WHITENING AGENTS, ABRASIVES, ALCOHOL AND HYDROCARBON PERFUMES AND OILS, ETC.
KEYS SURFACTANTS, DETERGENTS, ENVIRONMENTAL IMPACT
CODE 7040F
- AUTH FALLON M., STARR R.
TITLE A PARADOXICAL APPROACH FOR DISPERSION OF OIL AT SEA
PUBL OCEAN ENGINEERING, VOL. 3, 1974
ABST OIL SPILLED AT SEA SPREADS INTO AN IRREGULAR OIL MASS. WAVES AND SEA TUNDOLINE BEAT PERTURBS OF THE OIL MASS INTO PARTICLES AND DRIVE THEM TO SUBSURFACE LAYERS. THIS PHENOMENON IS CALLED DISPERSION AND IS DISCUSSED HERE.
KEYS DISPERSION, TURBULENCE FLUCTUATIONS, WAVE ACTION
CODE 8504F
- AUTH FALLON M., STARR R.M.
TITLE MOVEMENT OF SPILLED OIL AT SEA
PUBL MARINE TECHNOLOGY SOCIETY JOURNAL, VOL. 10, NO. 1, JAN. 1970
ABST THIS PAPER PROVIDES AN OVERVIEW OF SOME IMPORTANT FACTORS ON THE MOVEMENT OF SPILLED OIL ON WATERWAYS. SPREADING, DRIFT, DIFFUSION, DISSIPATION
KEYS
CODE 8501F
- AUTH FALLON-BROWNE M.
TITLE RANDOM-WALKS OF SPILLED OIL MOVEMENT
PUBL UNIVERSITY MICROFILMS INTERNATIONAL, ANN ARBOR, MICH.
ABST THIS DISSERTATION FOCUSES UPON MODELING THE DOMINANT FORCES OF MOVEMENT OF SPILLED OIL IN AN UNCONTAMINATED ENVIRONMENT. REVIEWING THE STATE OF THE ART, IT IS CONCLUDED THAT A CAUSAL ANALYSIS OF THE RANDOM MOVEMENT OF SPILLED OIL IS BEYOND THE SHORT TERM REACH. A SEMI-EMPIRICAL MODELING APPROACH WITH PARALLEL FLOW DETERMINING INITIAL EFFECTS OF RANDOM ENVIRONMENTAL INFLUENCES IS SUGGESTED.
CODE 85124F
- AUTH FANNELOP T.R., WALDRON G.D.
TITLE THE DYNAMICS OF OIL SLICKS
PUBL PAPER NO. 72-16, AIHA, BOSTON 1971
CODE 2090F
- AUTH FANTASIA J., INKHAL M.
TITLE THE DEVELOPMENT OF AN EXPERIMENTAL AIRBORNE LASER OIL SPILL REMOTE SENSING SYSTEM
PUBL DETECTION AND MONITORING OF SPILLS
ABST THE DEVELOPMENT AND LAB TESTS RESULTS OF THE EXPERIMENTAL SYSTEM ARE DESCRIBED.
KEYS DETECTION, CLASSIFICATION, QUANTIFICATION
CODE 0811F
- AUTH FARLOW J.S., FREESTONE F.J.
TITLE OPERATION OF NEW EPA FACILITY PERMITS TEST OF OIL-SPILL CLEANUP EQUIPMENT
PUBL OIL AND GAS JOURNAL, JUNE 30, 1975
ABST A REPORT ON THE OPERATION OF A NEW OIL AND HAZARDOUS MATERIALS SIMULATED ENVIRONMENTAL TEST TANK THAT IS AVAILABLE ON A COST-BASIS. TO OBTAIN PRIVATE AND GOVERNMENT USERS TO CONDUCT TESTS AND TO DEVELOP FULL SIZE DEVICES AND TECHNIQUES FOR CONTROL OF OIL AND HAZARDOUS MATERIALS SPILLED IN INLAND AND COASTAL WATERS.
KEYS CLEANUP, WAVE AND TIDE SPILLS, OIL AND HAZARDOUS MATERIALS SIMULATED ENVIRONMENTAL TEST TANK
CODE 2007F
- AUTH FARLOW J.S., FREESTONE F.J.
TITLE USEPA'S TEST FACILITY OPERATES: THE FIRST SEA MONITORING EXPERIENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
ABST A REPORT OF THE FIRST SEA MONITORING TEST TANK OPERATION AND A DISCUSSION OF THE FEASIBILITY OF THE FACILITY'S SERVING THE PUBLIC AND PRIVATE USERS IS PRESENTED.
KEYS CLEANUP, BIOLOGICAL IMPACT, PREVENTION
CODE 0527F
- AUTH FARRELL C.
TITLE DISCUSSION OF DYNAMICS OF CONTAINED OIL SLICKS
PUBL JOURNAL OF THE HYDRAULIC DIV., ASCE, VOL. 95, NO. MY PROL. PAPER 5023, JULY 1971
CODE 0720F
- AUTH FARRINGTON J.W., REEDERS G.V.
TITLE EVALUATION OF SOME METHODS OF ANALYSIS FOR PETROLEUM HYDROCARBONS IN MARINE ORGANISMS
PUBL GEOGRAPHIC INSTITUTE, WOODS HOLE, EPA 1975 CONFERENCE
KEYS ANALYSIS, MARINE ORGANISMS, HYDROCARBONS
CODE 8083H
- AUTH FAY J., MCKENZIE J.
TITLE CO2 CRACK
PUBL ENVIRONMENT, VOL. 24, NO. 9, NOV. 1972
ABST IMPACTATION OF LIQUIFIED NATURAL GAS MAY HELP MEET RISING ENERGY NEEDS IN THE US BUT MAY CREATE NEW SAFETY HAZARDS. ARTICLE INCLUDES STATISTICS ON IMPORTATION QUANTITIES OF NATURAL GAS AND PROPERTIES OF NATURAL GAS SPILLS.
CODE 3095F
- AUTH FAY J.A.
TITLE OIL SPILL: THE NEED FOR LAW AND SCIENCE
PUBL TECHNOLOGY REVIEW, VOL. 72, NO. 3, JAN. 1970
ABST THE CONTROL OF MARINE OIL POLLUTION IS HAMPERS BY INADEQUATE RESEARCH AND BY ECONOMIC CONSTRAINTS.

- AUTH ERLING BRATBERG
 TITLE THE BRAVO OILS OUT
 PUBL INSTITUTE OF MARINE RESEARCH, SER. B, NO. 5, MAY 1977
 ABST A REPORT ON MARINE RESEARCH ACTIVITIES APRIL 23 TO MAY 5, 1977 INCLUDING SOME PRELIMINARY RESULTS.
 REYN PLATFORM/BLOWOUT, DISCHARGES, TOXICITIES
 CODE 0504F
- AUTH ESTES J.E., GOLUMB D.
 TITLE OIL SPILLS: REFINED PUM MEASURING THEIR EXTENT ON THE SEA SURFACE
 PUBL SCIENCE, VOL. 186, AUG. 1970
 ABST THIS PAPER DISCUSSES AN ACCURATE SYSTEM DEVELOPED TO MEASURE SPILLS.
 REYN AREA AFFECTED, DEGREE OF CONCENTRATION, QUANTITY OF POLLUTANTS
 CODE 2101F
- AUTH ESTES J.E., THARAN M.R., SINGER L.W., MINULAN P.G.
 TITLE VOLUMETRIC DETERMINATION OF MARINE OIL SPILLS USING COORDINATED AIRBORNE AND SURFACE SURVEILLANCE DATA
 PUBL DETECTION AND MONITORING OF SPILLS
 ABST THIS PAPER DISCUSSES A SYSTEM FOR ESTIMATING THE VOLUME OF OIL LOSS RESULTING FROM OIL POLLUTION INCIDENTS.
 REYN DETECTION, MEASUREMENT, MONITORING
 CODE 0840F
- AUTH EVANS J.T.
 TITLE PNEUMATIC AND SIMILAR BLOWERS
 PUBL DOCKS AND BRITISH TRANSPORT COMMISSION, WATERWAYS RESEARCH STATION, JUNE 1955
 ABST THE SURFACE CURRENTS SET-UP BY AIR INJECTION AND THE DISTRIBUTION OF THE WATER VELOCITY WITHIN THE CURRENTS, CAN BE MATCHED BY CURRENTS SET UP BY WATER JETS AND THAT THE TWO CURRENTS DO MATCHED HAVE ALMOST THE SAME WATER-DAMPING EFFECTS WHETHER THEY ARE SET UP BY WATER JETS OR AIR. IT IS FOUND THAT WAVES OF SMALL AMPLITUDE ARE STOPPED IN THE WAY PREDICTED THEORETICALLY.
 REYN SURFACE CURRENTS, WATER VELOCITY, WATER JETS.
 CODE 3019F
- AUTH EWING G.
 TITLE SLICKS, SURFACE FILMS, AND INTERNAL WAVES
 PUBL JOURNAL OF MARINE RESEARCH, VOL. 23, NO. 3, 1950
 ABST THIS PAPER DISCUSSES THEORIES AND TESTS OF THE RELATION OF SLICKS TO WAVE MOTION.
 REYN RIPPLE-DAMPING, COMPACTUM, WIND STRESS
 CODE 0327F
 BUT PROPERLY DESIGNED LEGISLATION COULD BE MADE TO DISCOURAGE THE POLLUTER.
 CODE 3043F
- AUTH FAY J.A.
 TITLE PHYSICAL PROCESSES IN THE SPREAD OF OIL ON A WATER SURFACE
 PUBL PHYSICAL PROCESSES
 ABST THIS PAPER REVIEWS OUR CURRENT UNDERSTANDING OF THE PHYSICAL PROCESSES WHICH INITIALLY CAUSE ULTIMATELY TERMINATE THE SPREAD OF OIL ON THE SURFACE OF WATER.
 REYN PHYSICAL PROCESSES, SPREADING, WATER SURFACE
 CODE 0506F
- AUTH FAY J.A.
 TITLE THE SPREAD OF OIL SLICKS ON A CALM SEA
 PUBL OIL ON THE SEA, PENNUP PRESS, 1969
 ABST THIS ARTICLE DEALS MATHEMATICALLY WITH OIL SLICK SPREADING.
 REYN MATHEMATICAL, SPREADING
 CODE 3044F
- AUTH FELDMAN R.H.
 TITLE PETROLEUM WEATHERING: SOME PATHWAYS, FATE AND DISPOSITION ON MARINE OILS
 PUBL NATIONAL ENVIRONMENT RESEARCH CENTER, OFFICE OF RESEARCH AND DEVELOPMENT, PROGRAM NO. 18A025, SEPT. 1973
 ABST THREE MECHANISMS OF WEATHERING OF OIL POLLUTION IN MARINE WATERS ARE DISCUSSED. PHOTOLYSIS, INTERACTION WITH TRACE MATERIALS AND SEDIMENTATION WITH PARTICULATE MATERIALS ARE CONSIDERED AS COMPETITIVE TO OTHER FATE OF PETROLEUM MECHANISMS AND AS HAVING POSSIBLE ECOLOGICAL IMPORTANCE.
 REYN WEATHERING, FATE, DISPOSITION, PHOTOLYSIS, TRACE MATERIALS, SEDIMENTATION
 CODE 0130F
- AUTH FELDMAN R.H.
 TITLE THE 90 MILE BALLAST OIL DUMPING PROHIBITED ZONE OFF ALASKA RECONSIDERED IN THE LIGHT OF AVAILABLE DATA CLEANED FROM SIGNIFICANT INCIDENTS
 PUBL US DEPT. OF INTERIOR, PNOA, OCT. 1970
 ABST DISCUSSION OF PETROLEUM POLLUTION IN THE ALASKAN ENVIRONMENT INFORMATION DEFICIENCIES FOR ANALYSIS OF THE ALASKAN SITUATION DISCUSSION OF THE 90 MILE PROHIBITED ZONE AND REFERENCES.
 CODE 0012F
- AUTH FERNANDES J.M.
 TITLE ENERGY CONSERVATION AND THE POTENTIAL ROLE OF WASTE
- PUBL US/JAPAN CONSERVATION SEMINAR, FEB. 4-5, 1974
 ABST THIS PAPER WILL TOUCH ON THE ENERGY CRISIS DISCUSS THE AVAILABILITY OF FUEL CONSIDER SOME OF THE TRADE OFFS AND LEAD INTO THE POSITION WASTE COULD TAKE IN A PROGRAM OF FUEL CONSERVATION.
 CODE 2963F
- AUTH FERRARI D.
 TITLE OUTBOARD'S INEFFICIENCY IS A POLLUTION FACTOR
 PUBL NATIONAL FISHERMAN, APRIL 1970
 ABST THE POLLUTION EFFECTS OF OUTBOARD MOTORS, THEIR SPILLAGE RATES AND WASTAGE ARE DISCUSSED.
 CODE 3044F
- AUTH FINKL L., BLACKLAD J.
 TITLE OIL SPILL TREATING AGENTS
 PUBL API, CONTRACT NO. 212800000, PROJECT OS-6, AL. 4150, REVISED 1977
 ABST TO UPGRADE INFORMATION REGARDING AVAILABLE OIL SPILL TREATING AGENTS.
 REYN TREATING AGENTS, WAREHOUSED MATERIALS, PRODUCTION RATES, READY REFERENCE
 CODE 0039A B
- AUTH FINNAN R., ROSS C.W.
 TITLE OIL SPILL BIBLIOGRAPHY MARCH, 1975 TO DEC. 1976
 PUBL RESEARCH AND DEVELOPMENT DIVISION, ENVIRONMENTAL EMERGENCY BRANCH, DEPT. OF FISHERIES AND ENVIRONMENT, EPA-HEC-77-10, FEB. 1977
 ABST PERTAINING TO THE FIELD OF OIL SPILLS, THIS BIBLIOGRAPHY REPRESENTS A LISTING OF VARIOUS LITERATURE EITHER WRITTEN OR PUBLISHED DURING THE PERIOD OF MARCH 1975 TO DEC. 1976.
 REYN BIBLIOGRAPHY, RESEARCH
 CODE 7151F
- AUTH FINGER S., TU Y.S.
 TITLE ANALYTICAL EXAMINATION OF OIL/WATER SEPARATION BY COALESCENCE
 PUBL CONTROL TECHNOLOGY RESEARCH AND DEVELOPMENT
 ABST THIS INVESTIGATION PROVIDES A BASIS FOR FUTURE LARGE SCALE ON SHIPBOARD STUDIES TO IMPROVE THE PERFORMANCE OF OIL/WATER SEPARATION OF OIL FROM OILY WATER MIXTURES.
 REYN COALESCENCE, SEPARATION, CLEANUP
 CODE 5117F
- AUTH FIDCUK A.J., BIELLEY V.B.
 TITLE SLOP TANK DESIGN FOR IMPROVED LOAD ON TOP.
 PUBL NAVAL RESEARCH AND ENGINEERING CO.
 ABST THIS INVESTIGATION PROVIDES A BASIS FOR FUTURE LARGE SCALE ON SHIPBOARD STUDIES TO IMPROVE THE PERFORMANCE OF SLOP TANKS ON EXISTING TANKERS AS WELL AS ON FUTURE TANKERS.
 REYN SLOP TANKS, LOAD ON TOP, TANKERS
 CODE 8043F
- AUTH FISHER P., STEVENSON A.
 TITLE NATIONAL HYDROCARBON SEEPS ALONG THE NORTHERN SHELF OFF THE SANTA BARBARA BASIN, CALIFORNIA
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1730, APR. 29-MAY 2, 1973
 ABST THIS PAPER DISCUSSES THE STUDY OF SEEPS ALONG FLOOR OF OCEAN.
 REYN SUB-BOTTOM PROFILER SYSTEM, HYDROCARBON SEEPS, SEDIMENTS
 CODE 0849F
- AUTH FORDS J.M.
 TITLE METHOD DEVELOPMENT AND INITIAL EVALUATIONS OF LARVAL LOBSTER EXPOSURE TO SOUTH LOUISIANA CRUCE OIL
 PUBL API, FEB. 20, 1976
 ABST THIS PAPER DISCUSSES THE RESULTS OF TESTS OF LOBSTER LARVAE TO OIL.
 REYN LARVAL LOBSTER EXPOSURE, TOXICITY, LOUISIANA CRUCE
 CODE 2955F
- AUTH FORRESTER D.D.
 TITLE DISTRIBUTION OF SUSPENDED OIL PARTICLES FOLLOWING THE GROUNDING OF THE TANKER ARGO
 PUBL JOURNAL OF MARINE RESEARCH VOL. 28-29
 ABST THIS PAPER DISCUSSES THE ORIGIN OF THE PARTICLES, THEIR DISTRIBUTION IN SIZE AND DEPTH AND TRANSFER.
 REYN FOOD CHAINS, DISPERSION, CIRCULATION
 CODE 0645F
- AUTH FOSSBERG R.A.
 TITLE FLEXIBLE OIL BOOM
 PUBL OFFICIAL GAZETTE OF THE US PATENT OFFICE, VOL. 924, NO. 2
 ABST DESCRIBES A NEW BOOM PRODUCT.
 CODE 3115A
- AUTH FOUKE, W.B., ZILLIQUÉ E.J., GARVIN J.A.
 TITLE USING ARTERIA TO ASSEY OIL DISPERSANT TOXICITIES
 PUBL WATER POLLUT. CONTROL FED. JOURNAL, 45(11):2309-2391
 CODE 1971F
- AUTH FOWLER J.R.
 TITLE MATHEMATICAL MODEL OF THE TEXAS A&M LOW TENSION OIL CONTAINMENT BARRIER
 PUBL PhD THESIS A&M UNIVERSITY
 CODE 20664F

- AUTH FUMLER J.R., BAILEY E.S.
 TITLE DYNAMIC RESPONSE OF SURFACE-MOUNTED VERTICAL BARRIERS TO WAVE ACTION BY ANALOG AND DIGITAL SIMULATION
 PUBL JOURNAL OF ENG. FOR INDUSTRY, FEB. 1974
 ABST A TWO-DIMENSIONAL THEORETICAL MODEL REPRESENTING THE DYNAMICS OF AN OIL CONTAINMENT BARRIER WAS SIMULATED ON ANALOG AND DIGITAL COMPUTERS.
 REYN MECHANICAL BARRIERS, CONTAINMENT, RESPONSES TO WAVES
 CODE 08347
- AUTH FRANKIS J.R.
 TITLE WIND STRESS ON A WATER SURFACE
 PUBL UNKNOWN
 ABST THIS REPORT SUMMARIZES THE ATTEMPTS AT MEASUREMENT OF TANGENTIAL STRESS OF WIND ON WATER SURFACES.
 REYN WINDSTRESS, WINDSPEED, DRAG, TANGENTIAL STRESS
 CODE 08677
- AUTH FRANKS R.L.
 TITLE OIL POLLUTION CONTROL ON THE BUFFALO RIVER
 PUBL UNKNOWN
 ABST THIS PAPER DISCUSSES THE TWO MAIN SYSTEMS DEVELOPED: THE UPPER RIVER SYSTEM AND THE LOWER RIVER SYSTEM. THE BASIC DESIGN OF THE AIR BARRIER IS DISCUSSED ALONG WITH THE RESULTS OF LAB. AND FIELD TESTS.
 REYN CONTROL, AIR BARRIERS, OIL RETRIEVAL, CHEMICAL USE
 CODE 09147
- AUTH FRANKS, U.
 TITLE IDENTIFICATION OF PETROLEUM OILS BY FLOURESCENCE SPECTROSCOPY
 PUBL INDUSTRIAL WASTE TREATMENT LAB., EPA, 1975
 CONFERENCE IDENTIFICATION, FLOURESCENCE SPECTROSCOPY
 CODE 00794
- AUTH FRANKENFELD J.W.
 TITLE FACTORS GOVERNING THE RATE OF OIL AT SEA: VARIATION IN THE AMOUNTS AND TYPES OF DISSOLVED OR DISPERSED MATERIALS DURING THE WEATHERING PROCESS
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 CODE 02404
- AUTH FRANKENFELD J.W.
 TITLE IDENTIFICATION OF WEATHERED OIL FILMS FOUND IN THE MARINE ENVIRONMENT
 PUBL ERAUN
 CODE 09414
- AUTH FRANKENFELD J.W.
 TITLE WEATHERING OF OIL AT SEA
 PUBL NIS AD-787789, ESSO RESEARCH AND ENGINEERING CO., 9/73
 ABST A STUDY WAS CONDUCTED TO DETERMINE THE RATE OF PETROLEUM PRODUCTS DISCHARGED IN THE MARINE ENVIRONMENT AND TO DETERMINE THE MAGNITUDE OF THE MODEL IMPACT VARIABLES ON THE PHYSICAL AND CHEMICAL CHANGES WHICH OCCUR.
 CODE 31144
- AUTH FREESTONE F.J., ANDERSON A.A., TRICALOSI, A.P.
 TITLE U.S. EPA RESEARCH IN HIGH-SPEED DEVICES FOR THE RECOVERY OF THIN-FILM OIL SPILLS
 PUBL EPA, TETRADINE CORP., SCIENCE APPLICATIONS INC., FOR EPA 1975 CONFERENCE
 ABST MATERIAL IS PRESENTED ON THE RATIONALE FOR DEVELOPING THE DEVICES FOR THE TESTING TECHNOLOGY USED AND THE TEST RESULTS FOR EACH OF THE DEVICES. DEVELOPMENT, THIN-FILM OIL SPILLS, RECOVERY
 REYN CODE 01274
- AUTH FREESTONE F.J., TOORATH A.D.
 TITLE REVIEW OF USEPA RESEARCH IN OIL-WATER SEPARATION TECHNOLOGY
 PUBL USEPA FOR EPA 1975 CONFERENCE
 ABST THE USEPA HAS SPONSORED TWO SEPARATE RESEARCH CONTRACTS IN THE FIELD OF OIL-WATER SEPARATION FOR THE FISCAL YEAR 1974. THE RATIONALE FOR DEVELOPMENT OF EACH OF THESE DEVICES ALONG WITH DETAILED INFORMATION CONCERNING TEST RESULTS IS PRESENTED.
 REYN RESEARCH, OIL-WATER SEPARATION
 CODE 01314
- AUTH FRYE J.P.M.
 TITLE DEVELOPMENT OF MEMBRANE PROTECTIVE BARRIERS UTILIZING HYDROPHILES IN SPECIFIC ARRANGEMENTS
 PUBL WAI MARINE TECHNICAL REPORT SERIES NO. 24
 CODE 03704
- AUTH FRYE J.
 TITLE SOMETHING IS BEING DONE ABOUT OIL
 PUBL BOATING ZIFF CAVIS PUBL., APRIL 1968
 ABST A DISCUSSION OF LEGISLATION PASSED TO CURTAIL VIOLATIONS OF POLLUTION LAWS AS PERTAINS TO OIL SPILL AND SOME METHODS OF DETECTION AND REMEDIAL ACTION.
 CODE 80447
- AUTH FRYE J.
 TITLE
- TITLE SPOT B.S. RILES OFF DELAWARE EYED FOR SUPERPUMP
 PUBL NATIONAL FISHERMAN, OCT. 1972
 ABST ARTICLE ON HOW MAN MADE ISLANDS COULD PREVENT PUBLIC AND ENVIRONMENTAL NEEDS. POLLUTION PREVENTION MEASURES ARE LISTED.
 REYN SUPERPUMP, MAN MADE ISLANDS, ENVIRONMENTAL NEEDS, POLLUTION PREVENTION
 CODE 00254
- AUTH GALES E.L., BUSS J.A., BLEDSOE E.J.
 TITLE SIMULATION CONCEPTS FOR FISHERY SYSTEMS
 PUBL WASHINGTON SEA GRANT REPORT NO. 850-74 77-5, REPRINTED FROM: JOURNAL OF THE FISHERIES RESEARCH BOARD OF CANADA, VOL. 34, NO. 12, P. 2874-2881, 1977
 ABST PRESENTS AN ADVANCED COMPUTER TECHNIQUE (LENALE LIST) WHICH PERMITS THE INCLUSION OF COMPLEX TIME SIMULATIONS AND DATA STRUCTURE IN FISHERY MODELS WITH LITTLE ADDITIONAL EFFORT. EXAMPLES OF APPLICATION TO COMPLEX INFURNATION ARRAYS AND AN AGE-STRUCTURED MODEL ARE INCLUDED.
 REYN FISHERIES, POPULATION, COMPUTER PROGRAMS, MODELS
 CODE 77471
- AUTH GALVIN C.J.
 TITLE WAVE-HEIGHT PREDICTION FOR WAVE GENERATORS IN SHALLOW WATER
 PUBL US ARMY CORPS OF ENGINEERS, TECHNICAL MEMORANDUM NO. 4, MARCH 1964
 ABST THIS PAPER DISCUSSES TESTING OF A METHOD OF WAVE HEIGHT PREDICTION.
 CODE 30404
- AUTH GANONI D.S.
 TITLE SHIPOWNERS, MARINERS AND THE NEW LAW OF THE SEA
 PUBL FAIRPLAY PUBLICATION LTD.
 ABST THIS REPORT DISCUSSES THE EFFECTS OF TECHNICAL LEGAL AND POLITICAL CONSTRAINTS UPON THE TRADITIONAL USERS OF THE WORLD'S OCEANS.
 REYN SHIPOWNERS, MARINERS, POLITICAL CONSTRAINTS
 CODE 20047
- AUTH GARNER G.R., TELYCH P.P., ROGERSON P.P.
 TITLE MORPHOLOGICAL ANOMALIES IN ADULT OYSTER, SCALLOP, AND ATLANTIC SILVERSIDES EXPOSED TO WASTE MOTOR OILS
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 CODE 01374
- AUTH GARRETT W.D., BRAGIN V.
 TITLE DETERMINATION OF THE ATMOSPHERIC CONTRIBUTION OF PETROLEUM HYDROCARBONS TO THE OCEANS
 PUBL WORLD METEOROLOGICAL ORGANIZATION, ISBN 92-83-10440-9, MAR. NO. 442, 1974
 ABST THIS REPORT REVIEWS THE EXISTING KNOWLEDGE CONCERNING PETROLEUM HYDROCARBONS IN THE MARINE ATMOSPHERE AND PRELIMINARY BY WHICH THEIR FLUX FROM THE AIR TO SEA MAY BE DETERMINED.
 REYN ATMOSPHERIC POLLUTION, CONCENTRATION, TRANSPORT
 CODE 76027
- AUTH GARRETT W.D.
 TITLE CONTINENTAL AND COASTAL OIL POLLUTION ON WATER WITH MONOMOLECULAR SURFACE FILMS
 PUBL UNKNOWN
 ABST UNDER FAVORABLE CONDITIONS MONOMOLECULAR SURFACE FILMS CAN BE USED TO GUIDE, CONFINE AND CONDENSE PETROLEUM SPILLS ON WATER.
 REYN PREVENTION, CONTAINMENT, RECOVERY
 CODE 05237
- AUTH GARRETT W.D.
 TITLE IMPACT OF PETROLEUM SPILLS ON THE CHEMICAL AND PHYSICAL PROPERTIES OF THE AIR/SEA INTERFACE
 PUBL NAVAL RESEARCH LAB., DEPT. OF THE NAVY, PROJECT NO. BR 131-02-41-5607, FEB. 10, 1972
 ABST WEATHERING DISPERSION AIR/SEA DYNAMICS ULTIMATELY DEGRADE THE SPILL TO TANGIBLE LUMPS AND/OR STABLE WATER-IN-OIL EMULSIONS, BOTH WHICH HAVE LONG LIFE TIMES IN THE SEA. ALTHOUGH AN OIL SPILL CAN DAMP ITS ENVIRONMENT BY SLOWING PROCESSES AT THE AIR/SEA INTERFACE AND RESISTING INTERACTIONS BETWEEN THE OCEAN AND ATMOSPHERE, A MONOMOLECULAR OCEAN SURFACE FILM CAPABLE OF GLOBAL IMPACTS IS UNLIKELY.
 REYN WEATHERING DISPERSION, DEGRADATION, EMULSION
 CODE 60967
- AUTH GEORGE J. DAVID
 TITLE THE EFFECTS OF POLLUTION BY OIL AND OIL-DISPERSANTS ON THE COMMON INTERTIDAL POLYCHAETES, CIRRIPIFORMIA TENTACULATA AND CIRRIPIFORMIA CIRRIPIFORMIA
 PUBL JOURNAL OF APP. ECOL., VOL. 8, NO. 2, AUG. 1971
 ABST THIS PAPER DISCUSSES TEST RESULTS OF DISPERSANTS ON POLYCHAETES.
 REYN DISPERSANTS, TOXICITY, POLYCHAETES
 CODE 21307
- AUTH GEORGE J.E.
 TITLE SUBLETHAL EFFECTS ON LIVING ORGANISMS
 PUBL MARINE POLLUTION BULL.

- CODE 10478
- AUTH GERRAN J.M.
 TITLE U.S. COAST GUARD ARCTIC OIL POLLUTION PROGRAM
 PUBL OFFICE OF RESEARCH AND DEVELOPMENT, USCG, FOR EPA CONFERENCE 1975
 ABST PAPER INCLUDES: THE ARCTIC POLLUTION RESPONSE PROGRAM; FIELD EXPERIMENTS; HADRWARE EVALUATION TEST; CONTAINMENT DEVICES; RECOVERY DEVICE; PERSONNEL AND SUPPLY EQUIPMENT PERFORMANCE.
 KEYW ARCTIC POLLUTION, CONTAINMENT, RECOVERY
 CODE 0103R
- AUTH Geyer R.A., Sweet W.E.
 TITLE NATURAL HYDROCARBON SEEPAGE IN THE GULF OF MEXICO
 PUBL TRANSACTIONS GULF COAST ASSOCIATION OF GEOLOGICAL SOCIETIES, 2ND ANNUAL CONVENTION, OCT. 24-26, 1973
 CODE 0339F
- AUTH GIBBS C.F.
 TITLE A NEW APPROACH TO THE MEASUREMENT OF RATE OF DILUTION OF CAUDI OIL IN SEAWATER SYSTEMS
 PUBL CHEMINDRE NO. 3, 1972
 CODE 2079R
- AUTH GIBSON R.
 TITLE NON-TOXIC DISPERSANT COMBATS OIL SPILLS
 PUBL WORLD PETROLEUM, 00141
 CODE 2125R
- AUTH GILBERT R.U.
 TITLE ON THE ESTIMATION OF SPATIAL PATTERNS FOR ENVIRONMENTAL CONTAMINANTS
 PUBL STATISTICS SECTION, SYSTEMS DEPT., PACIFIC NORTHWEST LABORATORIES, BATTELLE MEMORIAL INSTITUTE, AUG. 1970
 ABST IN THIS PAPER THE PERFORMANCE OF AN ITERATIVE PROCEDURE FOR ESTIMATING THE GRID VALUES TO DETERMINE SPATIAL PATTERN OR GEOGRAPHICAL DISTRIBUTION OF ENVIRONMENTAL CONTAMINANTS IS EXAMINED.
 KEYW SPATIAL PATTERN, GEOGRAPHICAL DISTRIBUTION, ENVIRONMENTAL CONTAMINANTS
 CODE 1210F
- AUTH GILFILLAN E.S., VANDERMEULEN J.M.
 TITLE ALTERATIONS IN GROWTH AND PHYSIOLOGY OF SOFT-SHELLED CLAMS, RYE ARENARIA, CHRONICALLY FILLED WITH BUNKER C FROM CNEADABUETO BAY, NOVA SCOTIA, 1970-76
 PUBL JOURNAL OF THE FISHERIES, VOL. 95, NO. 5, MAY 1978
 ABST DATA ON CARBON FLUX AND SHELL AND TISSUE GROWTH, AND ON POPULATION STRUCTURE AND RECRUITMENT OF R. ARENARIA FROM CHRONICALLY FILLED SEWAGE TANKS & AN. 2 YEAR POSTSPILL RESULTS ARE DISCUSSED IN TERMS OF POPULATION RECOVERY POTENTIAL DURING CHRONIC OIL EXPOSURE.
 KEYW PHYSIOLOGY, GROWTH, CARBON FLUX, RECRUITMENT
 CODE 2680F
- AUTH GILMORE W.A., SMITH U.D., RICE A.M., SMENTON E.M., RUSER W.H.
 TITLE FINAL REPORT, SYSTEMS STUDY OF OIL SPILL CLEANUP PROCEDURES, VOL. 1, ANALYSIS OF OIL SPILLS AND CONTROL MATERIALS
 PUBL DILLINGHAM CORP., COMMITTEE FOR AIR AND WATER CONSERVATION API, FEB. 1970
 ABST THE INTENT OF THIS STUDY WAS TO PROVIDE MEMBERS OF THE PETROLEUM INDUSTRY WITH AN INDEPENDENT EXAMINATION OF THE MEANS CURRENTLY AVAILABLE FOR CONTROLLING SPILLS.
 KEYW CLEAN UP, CONTROL, RUGH WATER
 CODE 2304F
- AUTH GAY AND ASSOCIATES
 TITLE FINAL REPORT - MAJOR OIL SPILLS FROM TANKERS AND BARGES AND OTHER VESSELS IN US WATERS/ANALYSIS OF RECENT TRENDS AND PATTERNS
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 ABST AN INVESTIGATION OF OIL SPILLS DURING THE WINTER 1976-1977 AND COMPARISON WITH OTHER SPILLS SINCE 1964.
 KEYW TANKERS, BARGES, VESSELS, TRENDS
 CODE 7157F
- AUTH GAESER J.L.
 TITLE A DISCUSSION OF THE FUTURE OIL SPILL PROBLEM IN THE ARCTIC
 PUBL PHYSICAL-BIOLOGICAL EFFECTS
 ABST THIS PAPER DEFINES THE CAUSES AND EFFECTS OF THE POTENTIAL ARCTIC PROBLEM BY PRESENTING SOME OF THE EXISTING INFORMATION ON THE TOPIC.
 KEYW DISPERSION, EVAPORATION, SOLUTION, ABSORPTION, BIODEGRADATION, ULTRA-VIOLET OXIDATION
 CODE 0970F
- AUTH GAESER J.L.
 TITLE AN EFFECTIVE OIL SPILL CONTAINMENT RECOVERY SYSTEM FOR HIGH SEAS USE
 PUBL APPLIED CONTROL TECHNOLOGY
 ABST THE DEVELOPMENT AND TESTING OF A NEW OPERATIONAL OIL SPILL CONTAINMENT RECOVERY SYSTEM IS DISCUSSED.
 KEYW CONTAINMENT, RECOVERY, BOOM AND SKIMMER
- CODE 0810F
- AUTH MALSER J.L., VANCE C.P.
 TITLE A STUDY OF THE BEHAVIOR OF OIL SPILLS IN THE ARCTIC
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1552, MAY 1-3, 1972
 ABST THIS PAPER DISCUSSES THE LONG RANGE RESEARCH EFFORT TO STUDY OIL POLLUTION IN THE ARCTIC. SPREADING RATES, INTERACTION OF OIL AND ICE, ACTING EFFECTS, BURNING AND NATURAL ABSORBENTS
 CODE 0501F
- AUTH GLENN W.
 TITLE OIL POLLUTION OF RIVERS, METHODS OF ANALYSIS
 PUBL DEPT. OF ENVIRONMENT, SSIE NO. 004-527
 CODE 0480F
- AUTH GOLUBNO C., BAJOH C.W.
 TITLE COLLECTION OF GAS CHROMATOGRAPHIC FRACTION GAS ACTIVATED CARBON AND IDENTIFICATION BY INFRARED SPECTROSCOPY
 PUBL APPLIED SPECTROSCOPY VOL. 33 NOV. 2, 1979
 ABST A NOVEL METHOD FOR COLLECTING GAS CHROMATOGRAPHIC FRACTIONS IN COMMERCIALLY AVAILABLE TUBES OF ACTIVATED CARBON HAS BEEN DEVELOPED AND TESTED ON A NUMBER OF URBAN MIXTURES.
 KEYW GAS CHROMATOGRAPHY, FRACTIONS, SEPARATION
 CODE 7632F
- AUTH GOLUBNO, C.
 TITLE COLLECTION AND ANALYSIS OF TREATED AND UNTREATED OIL SPILL VAPORS
 PUBL A THESIS SUBMITTED IN PARTIAL FULFILLMENT OF THE REQUIREMENTS FOR THE DEGREE OF MASTER OF SCIENCE IN CHEMISTRY, APRIL 1976
 ABST THIS PAPER DISCUSSES THE CHEMICAL TREATMENT OF OIL SPILLS INVOLVING THE USE OF DISPERSANTS.
 KEYW DISPERSANTS, CHEMICAL TREATMENT
 CODE 7673F
- AUTH GOLDMAN J.J., BUNNELL J.
 TITLE FORECASTING AND HINDCASTING THE MAXIMUM COMBINE SEA IN SICRMS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1032, APR. 24-MAY 28, 1977
 ABST THIS PAPER DISCUSSES THE IMPORTANCE OF DETAILED WIND INFORMATION FOR BOTH FORECASTING AND HINDCASTING.
 KEYW FORECASTING/HINDCASTING, WIND, WAVES, SHELLS
 CODE 0847F
- AUTH GOLDSMITH R., MOSSMAN S.
 TITLE OIL WATER SEPARATION BY ULTRAFILTRATION
 PUBL CONTROL TECHNOLOGY RESEARCH AND DEVELOPMENT
 ABST THE OBJECT OF THIS REPORT IS TO DEVELOP TECHNOLOGY TO TREAT OIL WISCHANGES, TESTING OF METHOD, REMOVAL ULTRAFILTRATION, IS SHOWN.
 KEYW DISCHARGES, TREATMENT, REMOVAL, ULTRAFILTRATION
 CODE 3170F
- AUTH GOLDSTEIN R., MILLER P.
 TITLE FINAL REPORT, NUMERICAL MODEL FOR PREDICTION OF SURFACE CURRENTS IN THE OCEAN
 PUBL USCG, DEPT. OF TRANSPORTATION, NOVA-0005-0, MAY 1974
 ABST AN ENSEMBLE OF 126 OBSERVATIONS OF SURFACE CURRENTS ON THE WESTERN FLORIDA SHELF NEAR 87 DEGREES 30 FEET WEST, 25 DEGREES 30 FEET NORTH IS REPORTED.
 KEYW SURFACE CURRENT, PRECIPITATION, FLORIDA SHELF
 CODE 2544F
- AUTH GOUGH P.W.
 TITLE FLUIDIC VELOCITY SENSOR FOR GASEOUS EFFLUENTS
 PUBL ASME PUBL.
 ABST THIS PAPER DESCRIBES THE FLUIDIC VELOCITY SENSOR THE PURPOSE OF THE PAPER IS TO DESCRIBE THE SUBSEQUENT DEVELOPMENT OF THIS SENSOR AND ITS APPLICATIONS IN INDUSTRY FOR MEASUREMENTS OF THE TYPE REFERRED TO, IF ITS CHARACTERISTICS ARE USEFUL IN A SUITABLE MANNER.
 CODE 2900R
- AUTH GOODIER J.L., STEVENS J.L., BEARY D.W., McMAHAN, J.A., MZGOLLEN S.V.
 TITLE SPILL PREVENTION TECHNIQUES FOR HAZARDOUS POLLUTION SUBSTANCES
 EPA CONTRACT NO. 1-12-577
 ABST STUDY DESIGNED TO INVESTIGATE THE PREVENTION OF HAZARDOUS MATERIAL SPILLS, AND TO DETERMINE METHODS THAT WOULD PREVENT SUCH SPILLS FROM ENTERING A PUBLIC WATER COURSE.
 KEYW PREVENTION, HAZARDOUS MATERIALS, PUBLIC WATER COURSE
 CODE 0054R
- AUTH GOODIER J.L.
 TITLE FUTURE GUIDELINES FOR US DEEPWATER PORT DEVELOPMENT
 PUBL UNKNOWN
 ABST THIS PAPER DISCUSSES EXISTING US FACILITIES, ENVIRONMENTAL IMPACT, SITE SELECTION, CANAL HANDLING FACILITIES, MARINE TRANSPORT, LARGE BULK CARRIER, DEEPWATER PORT

- CODI 7166
 AUTH GARDNER P.C.
 TITL MEASUREMENT AND MOLECULAR INTERPRETATION OF SURFACE SHEAR VISCOSITY
 PUBL GEORGE W. WILSON, JR., TECHNICAL NOTE FOR US NATIONAL SCIENCE FOUNDATION
 CODE 0366
- AUTH GARDNER P.C., ALLEN L.A., PUSMANZER A.
 TITL A NEW SURFACE VISCOSITY OF HIGH SENSITIVITY I
 PUBL PREPRINT PAPER P.C. GARDNER
 CODE 0433
- AUTH GOS G., MATHEIAS J.
 TITL IECI CONFERENCE 1976
 PUBL PROCEEDINGS OF THE FIRST CONFERENCE OF THE EUROPEAN COOPERATION IN OCEANOGRAPHY
 CODE 35120
- AUTH GURJUN A., GERARD R.
 TITL WIND DRIFT SURFACE CURRENTS AND SPREAD OF CONTAMINANTS IN SHELL WATERS
 PUBL DEPT. OF TRANSPORTATION, USCG
 ABST THE RESULTS OF THE EXPERIMENTS INDICATE THE PRESENCE OF STAGNANT VERTICAL AND LATERAL SHEAR WITHIN THE UPPER FEW METERS OF THE WATER.
 REVD VERTICAL AND LATERAL SHEAR, WIND DRIFT, SPREAD OF CONTAMINANTS
 CODE 29424
- AUTH GURJUN A., GERARD R.
 TITL FINAL REPORT - WIND DRIFT SURFACE CURRENTS AND SPREAD OF CONTAMINANTS IN SHELL WATERS
 PUBL USCGA 40 703 107
 CODE 0393
- AUTH GORDON L.C., DALL J., KEIZER P.D.
 TITL IMPORTANCE OF SEDIMENT BURNING BY THE DEPOSIT-RELEASING POLYMERITE BARRIER MARINA ON THE WEATHERING RATE OF SEVENTEEN-BRAND OIL
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1976
 ABST THE INTERACTIONS BETWEEN THE POLYMERITE ANEMELLA MARINA A CURRENT DEPOSIT FIELDS IN SANDY INTERTIDAL AREAS, AND SEDIMENT CONTAMINATED WITH THE FRESH API REFERENCE OILS AND WEATHER NUMBER C OIL REMAINING FROM THE 1976 ARABIAN SPILL ARE INVESTIGATED IN LABORATORY EXPERIMENTS.
 REVD SEDIMENT, POLYMERITE, WEATHERING RATE
 CODE 26497
- AUTH GORDON R., SPAULDING R.
 TITL BIOGEOGRAPHY OF NUMERICAL MODELS FOR TIDAL RIVERS, ESTUARIES AND COASTAL WATERS
 PUBL USCG MARINE TECHNICAL REPORT NO. 22, OCEAN ENGINEERING AND SEA WORTHINESS, 1974
 ABST THIS PUBLICATION INCLUDES A DOCUMENT LISTING, A SELECTED REVIEW AND FOUR INDICES: REF NUM IN CONTEXT INDEX, AUTHOR INDEX, COMPUTE INDEX AND INVENTED INDEX.
 REVD BIOGEOGRAPHY, DOCUMENT LISTING, INDICES
 CODE 29297
- AUTH GOREN S.L.
 TITL REMOVAL OF OIL FROM AQUEOUS WASTES BY FILTRATION
 PUBL CALIF. RESOURCES CENTER
 ABST THE EFFECTS OF ELECTROLYTE TYPE AND CONCENTRATION ON THE SEPARATION OF OIL IN WATER DISPERSANTS WAS EXAMINED EXPERIMENTALLY.
 CODE 60979
- AUTH GURD J.R.
 TITL HAZARDS OF POLLUTION OF THE SEA
 PUBL HAZARDS OF MARITIME TRANSPORT, BALLINGER PUBLISHING CO., 1973
 ABST INCLUDES A BRIEF DISCUSSION ON OIL INSURANCE PROGRAMS FOR TANKERS AND A LISTING OF API PROJECTS ON OIL SPILL RESEARCH.
 CODE 31078
- AUTH GRABEL W., PHELPS V.
 TITL FAST CURRENT OIL CONTROL STUDY
 PUBL USCG, DEPT. OF TRANSPORTATION, REPORT NO. CG-0-8-75, INTERIA REPORT, AUG. 1974
 ABST A VORTEX RECOVERY DEVICE WAS CONCEIVED AND TESTED WHICH SHOWED ONLY VERY SMALL LOSS RATES AT ALL SPEEDS. RATE OF RECOVERY OF A SLICK INCREASED WITH CURRENT SPEED.
 REVD BARRIERS, FAST CURRENT OIL BEHAVIOR, HEADING, RATES OF RECOVERY
 CODE 60557
- AUTH GRAMER D.J.
 TITL FIELD EVALUATION OF OPEN SEA OIL SPILL RECOVERY EQUIPMENT
 PUBL NAVAL UNDERWATER SYSTEMS CENTER, TECHNICAL NOTE NO. 8-1330, FEB. 1974
 ABST DEPLOYMENT TEST OF TWO TYPES OF OIL CONTAINMENT BOOMS AND TWO OIL SKIMMERS WERE CONDUCTED.
 REVD OIL RECOVERY, DEPLOYMENT, OIL CONTAINMENT BOOMS, OIL SKIMMERS
 CODE 08097
- AUTH GRAMER D.J.
 TITL MULTICOMPONENT EVALUATION TEST OF HARBOR OIL SPILL RECOVERY SYSTEM
 PUBL TECHNICAL NOTE 8-1253, NAVAL CIVIL ENGINEERING LAB., JUNE 04223
 CODE 04223
- AUTH GRAMER D.J., SUMERS L.
 TITL EVALUATION TEST OF A SMALL HARBOR OIL SPILL RETRIEVAL SYSTEM
 PUBL NAVYING POLLUTION CONTROL CAMP., AD 782567, JULY 1975
 ABST DISCUSSION ON A SMALL TWO MAN SKIRREEN.
 CODE 31138
- AUTH GRAM-NIELSEN U., STAVELAND J.T., WILHELMSEN S.
 TITL ACIDIC HYDROCARBONS IN BENTHIC ORGANISMS FROM COASTAL AREAS POLLUTED BY IRANIAN CRUDE OIL
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1976
 ABST THIS INVESTIGATION WAS BEGUN ONE MONTH AFTER A SPILL OF 2000 TONS OF IRANIAN CRUDE OIL PULLED TO SHORES ALONG THE WEST COAST OF NORWAY IN FEB. 1976. IT IS BASED ON MASS-FRAGMENTOGRAPHIC ANALYSIS OF NAPHTHALENE, METHYL, DIMETHYL AND TRIMETHYLNAPHTHALENES, PHENANTHRENE, METHYL AND DIMETHYLPHENANTHRENE, DIBENZOTHIOPHENE, METHYL AND DIMETHYL AN, TRIMETHYLICENOTHIOPHENE.
 REVD BENTHIC ORGANISMS, NAPHTHALENES, MASS FRAGMENTOGRAPHY
 CODE 28697
- AUTH GRAY J.S.
 TITL PROGRAMME TO ASSESS THE ECOLOGICAL EFFECTS OF OIL SPILLS IN COASTAL AREAS OF NORWAY
 PUBL NORWEGIAN MARINE POLLUTION RESEARCH AND MONITORING PROGRAMME (POM)
 ABST THE PROGRAM DESCRIBED HERE IS DESIGNED TO ACQUIRE A QUANTITATIVE ASSESSMENT OF THE EFFECTS OF OIL ON SMALLER WATERS BIOTA AND COVERS THE WHOLE OF THE NORWEGIAN COAST.
 REVD OIL SPILL, CONTINGENCY, CHEMICAL ANALYSIS
 CODE 77427
- AUTH GRAY D.C.
 TITL THE 1972 IMO CONVENTION A TANKER OPERATORS VIEWPOINT
 PUBL GARON CORP.
 ABST THE ESSENTIAL PROVISIONS OF THE CONVENTION IS REVIEWED STRESSING THE TECHNOLOGY ELEMENTS RELATING TO OIL TANKERS, QUESTION OF RECEPTION FACILITIES ABOARD IS CONSIDERED.
 REVD TECHNOLOGY, OIL TANKERS, RECEPTION FACILITIES
 CODE 00716
- AUTH GREEN F.
 TITL SPAS VIEW OF PROPOSED OIL DRILLING ON THE CONTINENTAL SHELF
 PUBL SEA TECHNOLOGY, OCT. 1976
 ABST THIS PAPER DISCUSSES FUTURE DRILLING OFFSHORE.
 REVD OFFSHORE DRILLING, COASTAL ZONE
 CODE 23297
- AUTH GREGG M.
 TITL THE MICROSTRUCTURE OF THE OCEAN
 PUBL UMANN
 ABST THE TEMPERATURE AND SALINITY OF SEAWATER CAN ALSO BE MAPPED. SUCH MAPPINGS ARE HELD TO CLEAN AND THE SEA IS SO EFFECTIVELY STIRRED BY WINDS AND TIDES.
 REVD SALINITY, TEMPERATURE, SALINITY, MAPPINGS
 CODE 63037
- AUTH GRIFFITH E., LOGAN J.W.R.
 TITL OIL DISPERSANT TOXICITY
 PUBL MARINE POLLUTION BULLETIN, 46(1)90-93, 1973
 CODE 31264
- AUTH GRIFFIN L.F., CALDER J.A.
 TITL TOXIC EFFECT OF WATER-SOLUBLE FRACTIONS OF CRUDE, REFINED AND WEATHERED OILS ON THE GROWTH OF A MARINE BACTERIUM
 PUBL APPL. AND ENVIRONMENTAL MICROBIOLOGY, MAY 1977
 ABST THIS STUDY DEMONSTRATES THE TOXICITY OF THE WATERS OF SEVERAL OILS, INCLUDING CRUDE, REFINED AND WEATHERED, ON THE MOTILE MARINE BACTERIUM SERRATIA MARINDURUM. ADDITIONALLY, IT WAS FOUND THAT CHANGES IN TOXICITY WERE RELATED TO CHANGES IN ORGANIC NUTRIENT CONCENTRATION.
 REVD TOXICITY, WATER-SOLUBLE FRACTIONS, MARINE BACTERIA
 CODE 72077
- AUTH GRIFFIN P.J.
 TITL RESPONSE OF A NATURAL POPULATION OF MARINE METEROBIC BACTERIA TO A CRUDE OIL AND A DISPERSANT
 PUBL MASTERS THESIS IN MICROBIOLOGY UNIVERSITY OF BIRBEK ISLAND
 ABST MESO-SCALE (ENVIRONMENTALLY EXPOSED TESTING SYSTEM) AND LABORATORY SYSTEMS WERE EXAMINED USING VIABLE PLATE COUNT, MOST PROBABLE NUMBER, AND REPLICA PLATING TECHNIQUES TO DETERMINE THE EFFECTS OF RUWIT CRUDE OIL AND/OR CORREX 9527 ON BACTERIAL POPULATIONS.
 REVD DISPERSANT, MESO-SCALE SYSTEM, BACTERIAL
 CODE 77677
- AUTH GRIFFITH D.
 TITL INVESTIGATION INTO THE TOXICITY OF CORREX - A NEW

- PUBL OIL DISPERSANT
 DEP. AGRI-C. FISHERY LEAFLET, 6.
 CODE 1088R
- AUTH GRISCOM C.A. TIPPIE V.C.
 TITLE RHODE ISLAND AND OFFSHORE WILT DIGEST OF A WORKSHOP
 PUBL ITH. OF MARINE RESOURCES, WRI, SPI, 22-24, 1970
 ABST A DIGEST OF INFORMATION EXCHANGED DURING A WORKSHOP ON RHODE ISLAND AND THE OFFSHORE PETROLEUM INDUSTRY.
 REYN OFFSHORE EXPLORATION, TRANSPORTATION, LEASE AND SALES
 CODE 0511F
- AUTH GRIZZLE P.L., CULMERAN P.L.
 TITLE GEL ANALYSIS OF 6-PARAFFIN DISTRIBUTION IN CRUDE OILS AND TOPPED CRUDE OILS FOR OIL IDENTIFICATION
 PUBL USERDA, DEL/RI-77/12, OCT. 1977
 ABST THIS PAPER DISCUSSES THE ANALYSIS AND EVALUATION OF PARAFFINS OBTAINED IN OIL SAMPLES FOR THEIR IMPORTANCE IN OIL IDENTIFICATION.
 REYN PARAFFINS, OIL SAMPLES, OIL IDENTIFICATION
 CODE 7119F
- AUTH GWAD N.E., DISALVO L.F. MUNIER L.
 TITLE IDENTIFICATION AND POTENTIAL BIOLOGICAL EFFECTS OF THE MAJOR COMPONENTS IN THE SEAWATER TRACT OF A BUNKER FUEL
 PUBL BULLETIN OF ENVIRONMENTAL CONTAMINATION AND TOXICOLOGY, VOL. 14, NO. 9, 1975
 ABST THIS IS A REPORT ON THE COMPOSITION OF SEAWATER EXTRACT OF A BUNKER FUEL.
 REYN SEAWATER EXTRACT, BUNKER FUEL, SEAWATER SOLUBLE FRACTION
 CODE 2570F
- AUTH GUERIN R.P.
 TITLE ENERGY SOURCES OF POLYCYCLIC AROMATIC HYDROCARBONS ON KEDGE NATIONAL LAB., EPA, AND US ENDA
 PUBL ABST THIS PAPER DISCUSSES THE ENERGY SOURCES OF POLYCYCLIC AROMATIC HYDROCARBONS.
 REYN POLYCYCLIC AROMATIC HYDROCARBONS, COMBUSTION, COAL, OIL SHALE, CONCLUSIONS
 CODE 2679F
- AUTH GURIZ G.
 TITLE RESTORATION OF BEACHES CONTAMINATED BY OIL
 PUBL CONTRACT NO. 14-47-804, RESEARCH AND MONITORING EPA SPI, 1977
 CODE 0071F
- AUTH GUNTHER M.
 TITLE THEORETICAL AND EXPERIMENTAL EVALUATION OF OIL CONTROL DEVICES
 PUBL PHYSICAL REMOVAL
 ABST THIS PAPER DESCRIBES THE FIRST PHASES OF A PROGRAM AIMED AT PROVIDING A MEANS FOR EVALUATION OF EXISTING OIL CONTAINMENT DEVICES AND FOR IMPROVING BASIC DESIGN.
 REYN CONTAINMENT, CONTROL, DESIGN IMPROVEMENT
 CODE 0804F
- AUTH HADJICUP G.L.
 TITLE SUPERTANKER AND SUPER PORTS: A BIBLIOGRAPHY WITH ABSTRACTS
 PUBL REPORT FOR 1974 SUPERSEDES REPORT DATED OCT. 1973
 CODE 0343R
- AUTH HALE L.A.
 TITLE HYDRODYNAMIC EFFECTS OF AN OIL SLEEK MECHANICAL ENTRAPMENT DEVICES
 PUBL TEXAS A & M RESEARCH FOUNDATION AD 77026 FEB. 1974
 ABST THE OBJECTIVE OF THIS STUDY WAS TO INVESTIGATE THE BEHAVIOR OF AN OIL SLEEK UNDER THE INFLUENCE OF VARIOUS MECHANICAL CONTROL DEVICES.
 CODE 0094F
- AUTH HALE R.E., AUGLER B.A.
 TITLE THE ACOUSTIC PERFORMANCE OF PIPE LAGGING SYSTEMS
 PUBL ASME PUBL.
 ABST THIS PAPER PRESENTS SOME EXPERIMENTAL RESULTS FOR TYPICAL PIPE LAGGING CONFIGURATION. COMMENTS ARE ALSO MADE REGARDING CERTAIN PROBLEMS THAT EXIST IN SOME PERFORMANCE CHARACTERISTIC DATA REPORTED IN THE LITERATURE AND BY MATERIAL MANUFACTURERS.
 CODE 2906F
- AUTH HALSTED B.W.
 TITLE MARINE POLLUTION AND PHARMACEUTICAL SCIENTIST
 PUBL AMERICAN JOURNAL OF PHARMACEUTICAL EDUCATION
 CODE 1046R
- AUTH HANPSON C.R., MOUL E.T.
 TITLE NO. 2 FUEL OIL SPILL IN BOURNE, MASSACHUSETTS: IMMEDIATE ASSESSMENT OF THE EFFECTS ON MARINE INVERTEBRATES AND A 3 YEAR STUDY OF GROWTH AND RECOVERY OF A SALT MARSH
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST THIS PAPER DISCUSSES THE IMMEDIATE ASSESSMENT OF A SPILL AND A LONG TERM ASSESSMENT ON THE EFFECT ON MARINE LIFE.
 REYN SALT MARSH, EROSION, ALGAL, MARSH GRASS, INTERSTITIAL FAUNA, MARINE INVERTEBRATES
 CODE 2069F
- AUTH HANCOCK J.B., JENSEN D.
 TITLE WATERBORNE DEBRIS IN MARINE POLLUTION INCIDENTS
 PUBL BATTLE, CUMMINGS LABS, USCG, ENVIRONMENTAL AND TRANSPORTATION TECHNOLOGY DIV. FOR EPA 1975 CONFERENCE
 ABST CURRENT DEBRIS HANDLING PRACTICES ARE DESCRIBED ALONG WITH THE GENERAL HANDLING REQUIREMENTS NECESSARY FOR SPILL CLEANUP CONTINGENCY PLANNING. EFFECTS OF DEBRIS ON POLLUTION RESPONSE EQUIPMENT ARE CONSIDERED.
 REYN CLEANUP, DEBRIS, CONTINGENCY
 CODE 0097R
- AUTH HANLEY C.W.
 TITLE THE BULL OF THE MARINE INSURANCE INDUSTRY IN THE EMERGING REGIME OF THE OCEANS
 PUBL THE LAW OF THE SEA: BALLANTRAE PUBLISHING CO. 1974
 ABST THIS ARTICLE DEALS WITH THE FINANCIAL, LEGAL AND PHYSICAL PROBLEMS IN INSURING SUPERTANKERS AND THEIR CARGOES. IT ALSO LISTS THE PRINCIPAL PHYSICAL CONCERNS AS OF UNDISMISSED TOWERS.
 CODE 3102H
- AUTH HARR B.W.
 TITLE OIL RELEASE OIL SPILL
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. 4111-15-11 DEC. 1974
 CODE 0787R
- AUTH HARR B.W., JAMES R.P.
 TITLE ENVIRONMENTAL ASPECTS OF A TEXAS SUPERPORT
 PUBL UNKNOWN
 ABST THE OBJECTIVE OF THIS STUDY IS TO EVALUATE THE ENVIRONMENTAL IMPACT OF A SUPERPORT ON THE TEXAS COAST, BOTH THE HONGKONG SPILL IMPACT OF CONSTRUCTION AND OF OPERATION AND THE OIL SPILL IMPACT ON THE COASTAL ENVIRONMENT ARE INCLUDED IN THIS PROJECT.
 REYN SUPERPORT ENVIRONMENTAL ASPECT, CONSTRUCTION AND OPERATION
 CODE 7193F
- AUTH HANNA P., PALOUJILLET C.
 TITLE EFFECTS OF POLLUTANTS ON THE GROWTH OF ALGAL
 PUBL REPORT OF NER PROGRESS, FEB. 1972
 ABST THIS PAPER DISCUSSES THE STUDY UNDERTAKEN TO DETERMINE THE EFFECTS OF POLLUTANTS ON GROWTH RATES OF ALGAL.
 REYN GROWTH RATES, TURBIDITY, NUTRIENT CONCENTRATIONS
 CODE 2130F
- AUTH HANSEN J.A.
 TITLE LIGHTWEIGHT OIL CONTAINMENT SYSTEM LOW TENSION BARRIER SYSTEM
 PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. 7101274/001, 1973
 CODE 2005F
- AUTH HANSON J.W., KOCHIS D.M.
 TITLE OAKLAND ESTUARY OIL SPILL CLEANUP: A REVIEW OF A MAJOR OIL SPILL CLEANUP IN A TRASH-LADEN ESTUARY EMPHASIZING SMALL BOAT BOAT CLEANUP.
 PUBL SPILL OIL CC. FOR EPA 1975 CONFERENCE
 ABST THE REPORT INCLUDES A DAY BY DAY REVIEW OF THE CLEANUP EXPERIENCE AND AN EVALUATION OF PROCEDURES, EMPHASIZING PROBLEMS ENCOUNTERED IN CLEANUP OF OIL IN TRASH-LADEN WATERS.
 REYN CLEANUP, PROCEDURES, TRASH-LADEN WATERS
 CODE 0044F
- AUTH HARTY R.W.
 TITLE WATER RESOURCES RESEARCH COORDINATION IN NEW ENGLAND
 PUBL RI WATER RESOURCES CENTER FOR N.E. COUNCIL OF WATER CENTER DIRECTORS, JAN. 1973
 ABST THIS REPORT INVESTIGATES THE POTENTIALS AND FEASIBILITY OF COORDINATING WATER RESOURCE RESEARCH ON A NEW ENGLAND WIDE SCALE AND DEFINES THEREFOR GUIDING PRINCIPLES FOR OTHER MULTI-STATE REGIONS.
 REYN WATER RESEARCH COORDINATION, REGIONAL WATER RESEARCH, COORDINATION OF WATER RESOURCES
 CODE 0580F
- AUTH HARGRAVE B.T., REYNOLDS L.
 TITLE CRAWLING AND RESPIRATION AS INDICES OF SUBLETHAL EFFECTS OF OIL AND A DISPERSANT ON AN INTERTIDAL SMALL PLITICINE LITTELLA
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- AUTH HARGRAVE B.T., PHILLIPS L.A.
 TITLE ESTIMATES OF OIL IN AQUATIC SEDIMENTS BY FLUORESCENCE SPECTRAUSCOPY
 PUBL ENVIRONMENTAL POLLUTION, VOL. 8, NO. 3, APRIL 1975
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 CODE 3097R
- AUTH HARRISON E.

- TITLE BIOINDICATORS OF POLLUTION
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- AUTH HARRISON E.
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- AUTH HARVEY A., STORES V.
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KEYS CENTRIFUGATION, SEPARATING EMULSIONS, PURIFICATION
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- AUTH HARGOOD R.
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KEYS CLEANUP TECHNOLOGY, DISPERSANTS, BOOMS, SUPERTANKERS
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- AUTH HARTY L.P.
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- AUTH HAY A.
TITLE OIL AND THE SEA - THE ECOLOGICAL IMPLICATIONS OF A CONTROVERSIAL INVASION
PUBL MARINE TECH. SOCIETY JOURNAL, VOL. 8, NO. 8, JAN. 1974
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KEYS EVAPORATION, DISPERSION, BIODEGRADATION
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- AUTH HAY R.G.
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- AUTH HAYBY L.P.
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- AUTH HAZEL C.A.
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- AUTH HEALY R.J.
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- AUTH HELMICH J.P., RASBERRY S.U.
TITLE FINAL REPORT, ACTIVITIES OF THE NBS SPECTROCHEMICAL ANALYSIS SECTION JULY 1970 TO JUNE 1971
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ABST SPECTROCHEMICAL RESEARCH ACTIVITIES, IMPROVEMENTS IN EQUIPMENT AND APPLICATIONS, ESPECIALLY TO THE CERTIFICATION OF NBS STANDARD REFERENCE MATERIALS, ARE SUMMARIZED. LISTINGS ARE GIVEN FOR PUBLICATIONS AND 25 TALKS BY MEMBERS OF THE SECTION DURING THE YEAR.
KEYS SECTION PROGRAM, MICROANALYSIS, SPECTROCHEMICAL ANALYSIS
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- AUTH HELLERUST J.A., SWEATH A., GERVIS M., HUTCHINSON I., MANNING B.
TITLE EXPERIMENTAL CRUDE OIL SPILLS ON A SMALL SUBARCTIC LAKE IN THE MALDENZIE MOUNTAINS, N.W.T.: EFFECTS OF PHYTOPLANKTON, PERIPLHYTON AND ATTACHED AQUATIC VEGETATION
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KEYS ENVIRONMENTAL EFFECT, SUBARCTIC LAKES, PHYTOPLANKTON, PERIPLHYTON, VEGETATION
CODE 0062F
- AUTH HELLMAN M.
TITLE AGING OF CRUDE PETROLEUM IN WATER
PUBL ERDOL UND KUNDE-ERDGAAS- PETROCHEMIE
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- AUTH HELLMAN M.
TITLE THE BEHAVIOR OF CRUDE OIL ON WATER SURFACES AS INDICATED BY THE TEMPORAL CHANGES IN FLOW CHARACTERISTICS
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- AUTH HELLMAN M.
TITLE COMBATING OIL WITH CURRENT TOWNS, A LARGE SCALE TEST IN THE NORTH SEA
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- AUTH HELLMAN M., BRUJAS F.
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- AUTH MENAGER C., WELSH P.L., BLACKLAW J.K., SMITH J.D.
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PUBL PHYSICAL REMOVAL
ABST THIS PAPER REPORTS ON A COST EFFECTIVENESS ANALYSIS PERFORMED FOR EQUIPMENT MATERIALS AND TECHNIQUES APPLICABLE TO THE REMOVAL OR DISPERSAL OF SPILLED OIL ON OPEN WATER.
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- AUTH MENAGER C.M., SMITH J.D.
TITLE RECOVERY OF FLOTTING OIL
PUBL CONTRACT NO. 69-DI-0070, PROJECT ISUBOMEL, SPI, 1972
ABST CONCEPT EVALUATION, RECOVERY OF FLOTTING OIL USING POLYURETHANE PUMPSORBENT
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- AUTH NESS A., WHITE F.M.
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ABST THIS REPORT SUMMARIZES SOME OF THE WORK DONE OUT AT THE UMI, UP IN ITS SEA GRANT PROGRAM FOR MODELING AND UPDATES PART OF THE ENGINEERING EFFORT IN THIS DISCIPLINE.
KEYS ESTUARINE MODELING, NUMERICAL MODEL, CONVECTIVE/DIFFUSIVE EQUATION OF MASS CONSERVATION
CODE 2030F
- AUTH NESS A., WHITE F.M.
TITLE NUMERICAL MODEL OF NARRAGANSETT BAY
PUBL UMI, MARINE TECHNICAL REPORT NO. 20
ABST THE NUMERICAL MODEL WAS DEVELOPED TO PROVIDE INFORMATION CONCERNING THE TIDAL DYNAMICS OF THE BAY AND THE ACCOMPANYING CURRENTS AND FLOWS.
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CODE 0010H

- AUTH MICHEL P.
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- AUTH HILLIARD R.E.
 TITLE RECOVERY OF WASTE OIL USING FLOATING-TYPE SWIMMERS
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 ABST LUBRICANT LEAKAGE AND SPILLAGE THAT FINDS ITS WAY INTO THE PLANT SEWERS IS RECOVERED BY MEANS OF A LOGGON WITH FLOATING TYPE SWIMMERS. THE WASTE IS EVENTUALLY USED AS A FUEL AT THE PLANT OILER HOUSE. THUS, A SATISFACTORY AND ECONOMIC MEANS OF DISPOSAL IS PROVIDED IN ADDITION TO THE POLLUTION ABATEMENT ASPECT.
 REYN RECOVERY, LEAKS, FLOATING-TYPE SWIMMER
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- AUTH HINZE J.O.
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- AUTH HINANE P., SARAI F.
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- AUTH HODGSON R.U., MCINTYRE R.V.
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- AUTH HOFFMAN D., RELES R.
 TITLE ANALYSIS OF A STRATIFIED SAMPLE OF OCEAN WAVE RECORDS AT STATION "INDIA"
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 REYN SEABED DRIFTERS, SEDIMENTS, MARINE BIOLOGY
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- AUTH HOLLINGER J.P.
 TITLE THE DETERMINATION OF OIL SLICK THICKNESS BY MEANS OF MULTIFREQUENCY PASSIVE MICROWAVE TECHNIQUE
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 ABST THIS INTERIM REPORT DISCUSSES THE TECHNIQUE FOR REMOTE DETERMINATION OF THE THICKNESS AND VOLUME OF SEA SURFACE OIL SPILLS USING MULTIFREQUENCY MICROWAVE RADIOMETRY.
 REYN THICKNESS AND VOLUME OF OIL, MULTIFREQUENCY MICROWAVE, RADIOMETRY
 CODE 7208F
- AUTH HOLLINGER J.P.
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 REYN MICROWAVE RADIOMETRY, MULTIFREQUENCY PASSIVE MICROWAVE, CONTROLLED MARINE OIL SPILLS
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- AUTH HOLLINGER J.P., MENNELLA R.A.
 TITLE OIL SPILLS: MEASUREMENTS OF THEIR DISTRIBUTIONS AND VOLUMES BY MULTIFREQUENCY MICROWAVE RADIOMETRY
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- AUTH MOORE R.A.
 TITLE EFFECTS OF TORREY CANYON POLLUTION ON MARINE LIFE
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 ABST THE ARTICLE DESCRIBES THE EFFECT OF THE TORREY CANYON ACCIDENT ON THE MARINE LIFE AND DISCUSSES BRIEFLY THE METHODS USED FOR CLEAN-UP.
 REYN CLEANUP, TORREY CANYON, ACCIDENT, MARINE LIFE
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- AUTH MARIS R.W.
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- AUTH MAIT R.
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- AUTH MURNSTEIN G.
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 CODE 6293H
- AUTH MURRAY R.L., MURPHY R.L., STEWART S.
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- AUTH MURPHY G.
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 REYN PHYSICAL EFFECTS, RAIN, CALM NEAR-SURFACE WATER
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- AUTH MURPHY G.
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- AUTH MURPHY G.
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- AUTH MURPHY G.P.
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- AUTH MURPHY D.P.
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- AUTH MURPHY D.P.
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- AUTH MURPHY D.P., CROSS R.W., BELGIAN J.W., PULLER E.C., BYRNOLDS R.J.
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- AUTH HOUSTON C.M.
TITLE BIOLOGICAL DEGRADATION OF HYDROCARBONS IN WATER
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CODE U3224
- AUTH NORDHE A.M.
TITLE EXPERIMENTAL OIL BARRIERS
PUBL URI FOR USCG, SSIE NO. 62-38991-1
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- AUTH HUFFORD W., LEISSAUER E.M., BELSH J.P.
TITLE FINAL REPORT, MOVEMENT OF SPILLED OIL OVER THE
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DETERMINED FROM FIFTEEN POTENTIAL OIL DRILLING
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IMPACT ON THE REICHENBOLDT AND WATER MOVEMENT IN
THE AREA. THIS SECOND CONSIDERS THE INTERACTIONS
OF THE ENVIRONMENTAL PROCESSES IN FORECASTING THE
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NORTH PACIFIC, WATER MOVEMENT
CODE 25027
- AUTH HUFFORD W.L.
TITLE BIOLOGICAL RESPONSE TO OIL IN MARINE ENVIRONMENT
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CODE 00544
- AUTH MUGHS P.
TITLE A DETERMINATION OF THE RELATION BETWEEN WIND AND
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DRIFT AND GRADIENT WIND.
KEYO DRIFT GRADIENT WIND, SPEED AND DIRECTION
CODE 00697
- AUTH MUNT G., MURTON D., LEVINE J., MAYL G., DUNYAN
M., SHELLEY W., JEAN L., LANE R., JAMNISA R.
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PUBL STATE OF MAINE DEPT. OF EP, FOR EPA 1975
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ABST A PRELIMINARY REVIEW OF DATA, SUCCESSSES AND
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KEYO PASSIVE TAILING, DEVELOPMENT, IDENTIFICATION,
PHYLLOCTES
CODE 00604
- AUTH MUNT G.S.
TITLE THE POSSIBILITY OF IDENTIFYING MYSTERY OIL SPILLS
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- AUTH MUNT J.P., ORRILL T.
TITLE WATER QUALITY STUDY OF MOUNTAIN HARBOR, LONG
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CODE 04544
- AUTH HUTCHINSON T.C., PRELIMINARY
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VEGETATION, CANADIAN ARCTIC
CODE 01434
- AUTH MYLAND J.
TITLE A REVIEW OF OIL POLLUTING INCIDENTS IN AND AROUND
NEW ENGLAND
PUBL ENVIRONMENTAL RESEARCH LAB., EPA 400/3-77-004,
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KEYO DISCHARGE, NEW ENGLAND AREAS, CAUSES
CODE 72057
- AUTH MYLAND J., ROUGENSON P., GARDNER G.
TITLE A CONTINUOUS FLOW SYSTEM FOR THE EXPOSURE OF
MARINE ORGANISMS TO OIL
PUBL EPA, PROCEEDINGS OF 1977 OIL SPILL CONFERENCE,
MARCH 1977
ABST A CONTINUOUS FLOW-THROUGH BIOASSAY SYSTEM IS
DESIGNED FOR EXPOSING MARINE TEST ORGANISMS AND
THEIR VARIOUS LIFE STAGES TO OIL.
KEYO OIL BIOASSAY SYSTEM, CONTINUOUS FLOW, OIL
- CONTAMINATION
CODE 00607
- AUTH MYLAND J., SCHMIDTKE L.
TITLE PETROLEUM HYDROCARBONS AND THEIR EFFECTS ON MARINE
ORGANISMS, POPULATIONS, COMMUNITIES AND ECOSYSTEMS
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ABST ANALYSIS OF AVAILABLE DATA FROM BIOASSAYS
CONDUCTED ON ADULT STAGES OF A WIDE VARIETY OF
MARINE ORGANISMS REVEALS LETHAL EFFECTS FROM A
SMALL FRACTION OF PETROLEUM AND PETROLEUM
PRODUCTS IN THE 1 TO 100 PART PER MILLION RANGE.
KEYO LETHAL AND SUBLETHAL EFFECTS, ECOLOGICAL EFFECTS,
CONTROL
CODE 12047
- AUTH MYLAND J., MELZIAN B.D., GALLAGHER W., RUGERSON
P., BLAKE W.S.
TITLE A TECHNIQUE FOR THE REMOVAL OF DISSOLVED AND
DISPERSED HYDROCARBONS FROM BIOASSAY EFFLUENTS
PUBL USEPA ENVIRONMENTAL RESEARCH LABORATORY,
MARRAGANSETTI, RI
ABST A METHOD IS DESCRIBED FOR THE EFFICIENT REMOVAL OF
PETROLEUM DERIVED HYDROCARBONS FROM THE OIL
CONTAINING EFFLUENT OF CONTINUOUS FLOW THROUGH
OIL BIOASSAY SYSTEM.
KEYO ENVIRONMENTAL POLLUTANTS, FILTRATION TECHNIQUES,
FLOW THROUGH OIL BIOASSAY SYSTEM
CODE 12047
- AUTH IMBERGE J., FISCHER W.B.
TITLE SELECTIVE WITHDRAWAL FROM A STRATIFIED RESERVOIR
PUBL EPA, PROJECT NO. 1500C/J, DEC. 1977.
ABST THEORETICAL AND EXPERIMENTAL FLOW INTO A LARGE
SINK IN A LINEARLY DENSITY STRATIFIED RESERVOIR.
THE PRIMARY FOCUS IS ON PARTITIONING THE FLOW INTO
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WITHDRAWAL LAYER THICKNESS AS A FUNCTION OF THE
DISTANCE FROM THE SINK.
KEYO WITHDRAWAL LAYER THICKNESS, SINK, LINEARLY DENSITY
STRATIFIED RESERVOIR
CODE 00474
- AUTH INAMI NAGUS
TITLE PREVENTION OF DISCHARGED OIL IN THE SEA
PUBL J. PUBL. SOC. JAP., VOL 51, NO. 561
CODE 10044
- AUTH INSTITUTE OF PETROLEUM
TITLE A REVIEW OF MECHANICAL SYSTEMS FOR THE RECOVERY OF
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PUBL COORDINATING COMMITTEE FOR THE PREVENTION OF SEA
POLLUTION, APRIL 1974
ABST THIS REPORT REVIEWS AVAILABLE INFORMATION ON THE
TECHNIQUES AND EQUIPMENT INVOLVED IN THE
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KEYO MECHANICAL RECOVERY, CONTAINMENT, SKIMMING,
TRANSFER, STORAGE, LOGISTICS
CODE 05147
- AUTH JACKSON R.G.
TITLE OFFSHORE OIL POLLUTION: LAW AND ENFORCEMENT
PUBL EPA 1975 CONFERENCE
ABST THE GENERAL PURPOSE OF THIS STUDY IS TO COVER
BROADLY IN NON-TECHNICAL TERMS THE SALIENT ASPECTS
OF LAW AND ENFORCEMENT AS RELATED TO OFFSHORE OIL
POLLUTION SO AS TO ACHIEVE A PRACTICAL OVERALL
PERSPECTIVE.
KEYO LAW AND ENFORCEMENT, OFFSHORE
CODE 00694
- AUTH JAIN S.L.
TITLE LIMITATIONS TO LENGTH OF CONTAINED OIL SLICKS
PUBL DISCUSSION MARCH 1974
ABST THIS DISCUSSION SHOWS THAT THE SOLUTIONS FOR THE
SLICK PROFILES AND FOR THE CRITICAL SLICK VOLUME
CAN BE OBTAINED IN CLOSE FORM.
KEYO THERMAL REGIMES, DENSITY DIFFERENCES, SLICK VOLUME
CODE 05717
- AUTH JAMES P.M.
TITLE REVIEW OF OIL SPILL CLEANUP TECHNIQUES AND
EXPERIENCES
PUBL GULF OIL CO., MAY 15, 1964
ABST A REVIEW OF EQUIPMENT, MATERIALS, TECHNIQUES AND
PROCEDURES THAT HAVE ACTUALLY BEEN USED AND ARE
BEING USED FOR CLEAN-UP OF OIL SPILLS WHICH OCCUR
IN HARBORS AND INLAND WATERWAYS SPECIFICALLY
CONCERNING THOSE METHODS USED BY GULF OIL CO.
CODE 30074
- AUTH JAMES W.P.
TITLE ENVIRONMENTAL ASPECTS OF A SUPERTANKER PERI ON THE
TEXAS GULF COAST
PUBL TEXAS A&M UNIV. SEA GRANT PROGRAM, REPORT NO.
TAMU-SG-73-201, DEC. 1972
CODE 20044
- AUTH JAMES W.P., MARK W.B.
TITLE ENVIRONMENTAL IMPACT OF A SUPERTANKER PORT
PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1734,
MAY, 1973
ABST THIS PAPER DESCRIBES A STUDY OF THE ENVIRONMENTAL
ASPECTS OF AN OFFSHORE SUPERTANKER PORT.
KEYO WIND AND WATER CURRENT, SIZE OF SPILL, SEA
CONDITIONS

CODE 0960F

AUTH JASPER W., RIM T., WILSON W.P.

TITL DRUP SIZE DISTRIBUTION IN A TREATED GIL WATER SYSTEM

PUBL ASTM - TECHNICAL PUBLICATION 659.874
ABST AN EXPERIMENTAL STUDY WAS CONDUCTED TO DETERMINE THE DRUP SIZE DISTRIBUTIONS IN A DISPERSANT TREATED GIL WATER SYSTEM.

KEYS DISPERSANTS, DRUP SIZE, INTERFACIAL AREA

CODE 6598F

AUTH JASPER W.L.

TITL DRUP SIZE DISTRIBUTIONS IN A TREATED OIL-WATER SYSTEM

PUBL A THESIS SUBMITTED IN PARTIAL FULFILLMENT OF THE REQUIREMENTS FOR THE DEGREE OF MASTER OF SCIENCE IN MECHANICAL ENGINEERING
ABST THIS PAPER DISCUSSES DRUP SIZE DISTRIBUTIONS IN A TREATED OIL-WATER SYSTEM.

KEYS DRUP SIZE DISTRIBUTIONS, TREATED OIL-WATER SYSTEM

CODE 65984F

AUTH JEFFERIES W.P., JOHNSON W.

TITL PETROLEUM, TEMPERATURE AND TOXICANTS: EXAMPLES OF SUSPECTED RESPONSES BY PLANKTON AND BENTHOS ON THE CONTINENTAL SHELF

PUBL U.S. MARINE REPORT NO. 69, MARINE ADVISORY SERVICE PUBLICATIONS
ABST RESULTS OF TESTING ON PLANKTON AND BENTHOS ON PETROLEUM, TEMPERATURE AND TOXICANTS ARE DISCUSSED.

KEYS PETROLEUM, TEMPERATURE, TOXICANTS, BENTHOS, PLANKTON

CODE 1030F

AUTH JEFFERY P.G.

TITL LARGE-SCALE EXPERIMENTS ON THE SPREADING OF OIL AT SEA AND ITS DISAPPEARANCE BY NATURAL FACTORS

PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION, 1973
ABST THIS PAPER DESCRIBES THOSE CONSIDERATIONS THAT ARE OF IMPORTANCE IN UNDERSTANDING LARGE-SCALE OIL SPREADING EXPERIMENTS.

CODE 2643A

AUTH JEFFERY P.G., NICHOLS J.A.

TITL DISPERSANTS FOR OIL SPILL CLEAN-UP OPERATIONS AT SEA, ON COASTAL WATERS AND BEACHES

PUBL BARKER SPRING LABORATORY, DEPT. OF TRADE INDUSTRY, LA 10310P, 1973
ABST THIS PRESENT REPORT REPLACES REPORT NO. LR 142, NOV. 1972. THE FIRST PART OF THIS REPORT PROVIDES GENERAL BACKGROUND INFORMATION AND RECENT IDEAS CONCERNING THE FORMATION, COMPOSITION AND USE OF MATERIALS INTENDED TO DISPENSE OIL. THE FINAL PART LISTS ALL THOSE DISPERSANT MATERIALS THAT HAVE BEEN RECEIVED AT BARKER SPRING LABORATORY.

KEYS DISPERSANTS, CLEANUP, PREVENTION

CODE 2621F

AUTH JENSEN D.S.

TITL U.S. COAST GUARD FAST CURRENT OIL REMOVAL SYSTEM DEVELOPMENT PROGRAM

PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2147, MAY 5-8, 1975
ABST FIVE CONCEPTS TO CONTROL AND REMOVE OIL SPILLS IN WATER CURRENT VELOCITIES UP TO 10 KNOTS ARE PRESENTED.

KEYS CONTROL, REMOVAL, HEAD WAVE, INTERFACIAL INSTABILITIES

CODE 0532F

AUTH JENSEN D.S., HEATON D.J., LINDENRUTH W., BEALM R.L.

TITL ENERGY DISSIPATIVE DEVICES TO CONTROL OIL SPILLS IN FAST-CURRENT ENVIRONMENTS

PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
ABST A CONCEPT TO CONTROL AND REMOVE OIL SPILLS IN POTENTIAL WATER CURRENT VELOCITIES OF 10 KNOTS IS PRESENTED.

KEYS CONTROL, RECOVERY, REMOVAL

CODE 0526F

AUTH JOHNSON A., COOK P.U., WELSH D.B.

TITL MICROBIAL UTILIZATION OF CRUDE OIL APPL. MICROBIOL 23:1082

PUBL APPL. MICROBIOL 23:1082
CODE 9040F

AUTH JOHNSON A.M.

TITL DANISH SEABIRD DISASTERS IN 1972

PUBL MARINE POLLUTION BULL. 4:1011-114
CODE 1082F

AUTH JOHNSON E., BEANCI D., FARRELL J.

TITL THE DESIGN, DEVELOPMENT, TEST AND EVALUATION OF AN OPEN OCEAN OIL RECOVERY SYSTEM FOR USE IN WAVES

PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1995, MAY 6-8, 1974
ABST THIS PAPER PRESENTS THE RESULTS OF A PROGRAM CONDUCTED BY JOE SCIENTIFIC TO ESTABLISH THE REQUIREMENTS FOR AND THEN TO BUILD AND TEST AN OPEN OCEAN OIL RECOVERY SYSTEM FOR OPERATION IN HIGH WAVE ENVIRONMENTS.

KEYS RECOVERY, SEABIRDS, TESTING

CODE 0960F

AUTH JOHNSON J.C., MCALIFFE C.D., BROWN W.

TITL PHYSICAL AND CHEMICAL BEHAVIOR OF SMALL CRUDE OIL SPILLS ON THE OCEAN

PUBL JOE SCIENTIFIC CORP.
ABST THIS PAPER DESCRIBES THE RESULTS OF A SERIES OF RESEARCH OIL SPILLS IN THE NORTH ATLANTIC TO DETERMINE THE PHYSICAL AND CHEMICAL BEHAVIOR OF FRESH OIL SPILLS.

KEYS RESEARCH OIL SPILLS, TRACKING, DISPERSION

CODE 7350F

AUTH JOHNSON J.W., WARD M.C.

TITL MIXING AND DISPERSION BY WIND WAVES

PUBL DEPT. OF HEALTH, EDUCATION AND WELFARE, SEA, 138, ISSUE 5, GRANT 66-040, UNIVERSITY OF CALIF. HYDRA ENGINEERING LAB.
ABST CHARACTER AND NATURE OF ACTION WIND WAVES ON DISPERSION IS DISCUSSED.

KEYS WIND WAVE ACTION, DISPERSION, MIXING

CODE 0400F

AUTH JONES M.H.

TITL POLLUTION CONTROL IN THE PETROLEUM INDUSTRY

PUBL POLLUTION TECHNOLOGY REVIEW NO. 4, NOTES DATA COMP. PARA RIDGE, NJ, 1973
ABST THIS REPORT ATTEMPTS TO CLARIFY THE WAYS AND MEANS OPEN TO THE ALERT PETROLEUM REFINER WHO MUST KEEP HIS POLLUTION WASTES DOWN TO A MINIMUM.

KEYS EFFLUENT WASTES, BIODEGRADABILITY, DISCHARGE

CODE 4012F

AUTH JONES L.W.

TITL USE OF SULFUR FOR COUNTERING OIL SPILLS

PUBL AMLEC PRODUCTION CO., OFFICIAL GAZETTE FOR US PATENT OFFICE, VOL. 927, NO. 5, OCT. 25, 1974
ABST SULFUR IS SPREAD OVER THE SPILLED OIL TO HOLD THE OIL MASS TOGETHER AND PERMIT IT TO BE EASILY REMOVED.

CODE 3130F

AUTH JONES R.C.

TITL DISPOSAL OF OIL SPILL DEBRIS

PUBL USCG, BOSTON, MASS.
ABST A LANDFILL WAS DESIGNED AND CONSTRUCTED FOR THE DISPOSAL OF APPROX. 8,500 YARDS OF DEBRIS IN THE CLEANUP OF A MAJOR POLLUTION INCIDENT IN MASSACHUSETT BAY, RI. THE RESULTS TO DATE: NO INCREASE IN THE TOTAL ORGANIC CARBON OR PHENOLIC CONTENT.

KEYS LANDFILL, CLEANUP, DISPOSAL, ORGANIC CARBON, PHENOLIC CONTENT

CODE 008F

AUTH JONES W.T.

TITL AIR BARRIERS AS OIL SPILL CONTAINMENT DEVICES

PUBL SOCIETY OF PETROLEUM ENGINEERS OF AIME, NO. SPE 3000, U.S., 4-7, 1970
ABST THIS PAPER DISCUSSES AN EXPERIMENTAL INVESTIGATION OF AIR BARRIERS AS CONTAINMENT DEVICES.

KEYS AIR BARRIERS, CONTAINMENT, SURFACE CURRENTS

CODE 0077F

AUTH JOHNSON E., BRAGA L.

TITL COAST GUARD OIL POLLUTION CONTROL SYSTEMS

PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1994, MAY 6-8, 1974
ABST THIS PAPER DISCUSSES THE CHARACTERISTICS, VARIOUS EQUIPMENT, AND THE MAKE UP OF THE NATIONAL STRIKE FORCE.

KEYS AIR TRANSFER SYSTEM, BARRIERS, RECOVERY, AIRBORNE REMOTE SENSING

CODE 0524F

AUTH JOHNSON R.C.

TITL MARINE POLLUTION MONITORING

PUBL OCS SPECIAL PUBLICATION NO. 1974, 1974
ABST PROCEEDINGS CONTAIN LECTURES REPRESENTING PERTINENT SCIENTIFIC, ENVIRONMENTAL AND REGULATORY ASPECTS OF PETROLEUM HYDROCARBONS MEASUREMENTS AND SUMMARIES OF VARIOUS DISCUSSIONS AND PAPERS. INCLUDES SPECIFIC RECOMMENDATIONS FOR MARINE PETROLEUM MONITORING.

KEYS MARINE PETROLEUM MONITORING, SCIENTIFIC, ENVIRONMENTAL AND REGULATORY ASPECTS

CODE 2139A

AUTH KAISER R., JONES D., LAMP M.

TITL TRUPLER, STON AGHS, PENNSYLVANIA'S TOWNS CENTER

PUBL EPA, 1973 CONF.
ABST LARGEST INLAND OIL SPILL 6-8,000,000 GALLONS OF SLUDGE OIL WAS RELEASED FROM ITS WASTE HOLDING LAGOONS ON JUNE 22, 1972

CODE 0110F

AUTH KAISER R., MISALCZY G., CURTIS R.A., COLTON L.A.

TITL THE RECOVERY OF OIL FROM WATER WITH MAGNETIC FLUIDS

PUBL PHYSICAL RECOVERY
ABST A NOVEL METHOD OF OIL-WATER SEPARATION HAS BEEN DEVELOPED WHICH UTILIZES MAGNETISM TO SEPARATE THE TWO PRELIMINARY RESULTS AND ECONOMIC PROJECTIONS ARE THEN PRESENTED.

KEYS OIL-WATER SEPARATION, MAGNETISM, FERRO-FLUID RECOVER

- CODE 5114F
 AUTH KAISER R.C., VAN CLEEVE W.O.
 TITLE REMOVAL AND PROCEDURES FOR PREVENTING OIL POLLUTION FROM ONSHORE AND OFFSHORE FACILITIES
 PUBL OIL SPILL PREVENTION
 ABST THE ROLL OF DESIGN CRITERIA, PERSONNEL OPERATING PROCEDURES AND HUMAN ERROR IN SPILL PREVENTION ARE DISCUSSED AND FUTURE FACILITIES ARE POSTULATED.
 KEYW PREVENTION, ONSHORE, OFFSHORE
 CODE 0871F
- AUTH RANE J.
 TITLE RAYLEIGH WAVES AT THE CONTINENTAL MARGIN
 PUBL U.S. SCIENTIFIC REPORT NO. 6, JUNE 10, 1965
 ABST THIS REPORT INTRODUCES AN ELEMENTARY PROCEDURE FOR THE SOLUTION OF PROBLEMS INVOLVING THE DIFFRACTION OF VECTOR FIELDS. IN PARTICULAR, THE REPORT DISCUSSES THE PROPAGATION OF RAYLEIGH WAVES INCIDENT UNBIASEDLY UPON THE CONTINENTAL MARGIN.
 KEYW RAYLEIGH WAVES, DIFFRACTION OF VECTOR FIELDS, CONTINENTAL MARGIN
 CODE 7688F
- AUTH RAPLAN A.M.
 TITLE MICROBIAL DEGRADATION OF MATERIALS IN LABORATORY AND NATURAL ENVIRONMENTS
 PUBL DEVELOPMENTS IN INDUSTRIAL MICROBIOLOGY, VOL. 18, 1977
 ABST THIS PAPER DISCUSSES THE IMPORTANCE IN DEVELOPMENT OF MATERIALS BEING THE DETERMINATION OF THEIR BEHAVIOR UNDER STRESS.
 KEYW DEGRADATION, ENVIRONMENTAL STRESS, DEVELOPMENT OF MATERIALS
 CODE 4526F
- AUTH RABUSE N., DELVIGNE G., VREUGDENHIL C.M.
 TITLE MOMENTUM AND MASS TRANSFER ON STRATIFIED FLOWS
 PUBL Delft Hydraulics Lab.
 ABST RESULTS OF THIS STUDY SHOULD GIVE RELATIONS BETWEEN DENSITY GRADIENTS AND THE VERTICAL TRANSFER OF MOMENTUM AND MASS IN THIS TYPE OF FLOWS WHICH COULD BE USED IN A TWO-DIMENSIONAL MATHEMATICAL MODEL.
 KEYW MOMENTUM AND MASS TRANSFER, STRATIFIED FLOWS, DENSITY GRADIENTS, VERTICAL TRANSFER
 CODE 2573R
- AUTH RATO M., PHILLIPS D.
 TITLE ON THE PENETRATION OF A TURBULENT LAYER INTO STRATIFIED FLUID
 PUBL J. FLUID MECH. VOL. 37, PART 4, DEC. 1959-60
 CODE 2112R
- AUTH RAITZ E.
 TITLE REMOVAL OF OIL FROM UNDER PIERS.
 PUBL PROJECT NO. 13080/VP, SPA, URS, 1973
 CODE 4074R
- AUTH KAWAHARA F.
 TITLE CHARACTERIZATION AND IDENTIFICATION OF SPILLED RESIDUAL FUEL OILS BY GAS CHROMATOGRAPHY AND INFRARED SPECTROSCOPY
 PUBL JOURNAL OF CHROMATOGRAPHIC SCIENCE, VOL. 10, OCT. 1972
 ABST ANALYTICAL METHOD DEVELOPED RECENTLY AT THE ANALYTICAL QUALITY CONTROL LAB AND DESCRIBED FOR THE CHARACTERIZATION AND IDENTIFICATION OF HEAVY RESIDUAL FUEL OIL POLLUTANTS FOUND IN SURFACE WATERS.
 KEYW IDENTIFICATION OF OIL SPILLED, GAS CHROMATOGRAPHY, INFRARED SPECTROSCOPY
 CODE 1201F
- AUTH KAWAHARA F.
 TITLE TRACE ORGANIC COMPONENTS AS FINGERPRINTS IN GAS CHROMATOGRAPHIC IDENTIFICATION OF SPILLED ASPHALTS
 PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY, VOL. 10, AUG. 1976
 ABST THIS PAPER DISCLOSES THE FIRST SUCCESSFUL APPLICATION OF GAS CHROMATOGRAPHY-ELECTRON CAPTURE DETECTION IN THE ANALYSIS OF THE ORGANIC TRACE COMPONENTS PRESENT IN ASPHALTS AND ITS USEFULNESS IN PROVIDING IDENTIFICATION OF ASPHALT POLLUTANTS FOUND IN SURFACE WATERS.
 KEYW OIL IDENTIFICATION, GAS CHROMATOGRAPHY, ELECTRON CAPTURE DETECTION
 CODE 1202F
- AUTH KAWAHARA F., BALLINGER D.
 TITLE CHARACTERIZATION OF OIL SPILLS ON SURFACE WATERS
 PUBL IND. AND ENG. CHEM. RES. AND DEVELOP., VOL. 9, DEC. 1970
 ABST NUMEROUS UNIDENTIFIED OIL SAMPLES COLLECTED FROM THE SURFACE WATERS OF THE UNITED STATES WERE ANALYZED BY THE METHOD OF RATIOS OF IMPAIRED ABSORBANCE USING SIX WAVELENGTHS.
 KEYW CHARACTERIZATION, IDENTIFICATION, RATIO VALUES
 CODE 1225F
- AUTH KAWAHARA F., SANTER J., JULIAN E.
 TITLE CHARACTERIZATION OF HEAVY RESIDUAL FUEL OILS AND ASPHALTS BY IMPAIRED SPECTROPHOTOMETRY USING STATISTICAL DISCRIMINANT FUNCTION ANALYSIS
 PUBL ANALYTICAL CHEMISTRY, VOL. 46, FEB. 1974
 ABST THIS PAPER DESCRIBES THE USE OF IMPAIRED SPECTROPHOTOMETRY IN IDENTIFYING RESIDUAL FUEL
- OILS.
 KEYW IDENTIFICATION, IMPAIRED SPECTROPHOTOMETRY, CLASSIFICATION SAMPLES
 CODE 1203F
- AUTH KAWAHARA F., YANG Y.
 TITLE SYSTEMS CHEMICAL ANALYSIS OF PETROLEUM POLLUTANTS
 PUBL ANALYTICAL CHEMISTRY, VOL. 48, APR. 1976
 ABST THE APPLICATION OF AN ESTABLISHED MATHEMATICAL TREATMENT USEFUL FOR THE CHARACTERIZATION AND IDENTIFICATION OF PETROLEUM POLLUTANTS IS DESCRIBED.
 KEYW CHARACTERIZATION, IDENTIFICATION, IMPAIRED SPECTROPHOTOMETRY
 CODE 1231F
- AUTH KAWAHARA F.P.
 TITLE GAS CHROMATOGRAPHIC ANALYSIS OF MERCAPTANS, PHENOLS, AND ORGANIC ACIDS IN SURFACE WATERS WITH USE OF PENTAVALENT SULFONATE DERIVATIVES
 PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY, VOL. 5, NO. 5, MAY 1971
 ABST QUALITATIVE SEPARATION AND QUANTITATIVE DETERMINATION SAMPLING IS DISCUSSED
 KEYW DETECTION, IDENTIFICATION, SAMPLING
 CODE 1211F
- AUTH KEVIL B., MORSELEIGH R.
 TITLE BEHAVIOR OF OIL SPILLED UNDER FLOATING ICE
 PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
 ABST COOL ROOM EXPERIMENTS DESIGNED TO SIMULATE A HOT OIL SPILL UNDER ICE IS DEMONSTRATED.
 KEYW CLEANUP, BEHAVIOR OF OIL UNDER ICE, COOL ROOM EXPERIMENTS
 CODE 0856F
- AUTH KEITH V.F., PORVICELLI J.V.
 TITLE AN ANALYSIS OF OIL OUTFLOWS DUE TO TANKER ACCIDENTS
 PUBL 1973 PROCEEDINGS
 ABST ANALYSIS OF DATA PERTAINING TO OIL SPILLS ACCORDING CRITERIA OF AMOUNT, LOCATION, ETC.
 CODE 3137R
- AUTH KEIZER P.D., AMER T.P., DALE J., VANDERMEULEN J.M.
 TITLE RESIDUES OF BUNKER C OIL IN CHEDABUCTO BAY, NOVA SCOTIA, 6 YEARS AFTER THE ANKOR SPILL
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1976
 ABST AN EXTENSIVE SURVEY OF SURFICIAL EQUIPMENTS, INTER-TIDAL AND SUBLITTORAL, OF CHEDABUCTO BAY IN MAY 1976
 KEYW GAS LIQUID CHROMATOGRAPHY, FLUORESCENCE SPECTROSCOPY, POLYCYCLIC AROMATIC HYDROCARBONS
 CODE 2669F
- AUTH KENNEDY J.M., MERRILL E.G.
 TITLE THE BEHAVIOR OF OIL AND WATER DERIVED FROM ALCOHOL IMPAIRED AND MICROWAVE RADIOMETRIC MEASUREMENTS
 PUBL 1971 CONFERENCE
 CODE 2030R
- AUTH KENNEDY J.M., MERRILL E.G.
 TITLE OIL SPILLS, IN AND MICROWAVE PHOTOGAMMATIC ENGINEERING, VOL. 37, DEC. 1975
 CODE 0398R
- AUTH KENNEDY J.M.
 TITLE HELICOPTER TOW TESTS OF THE USCG'S AIR DELIVERY CONTAINER FOR OIL SPILL CONTAINMENT BARGE
 PUBL US NAVAL COASTAL SYSTEMS LAB., REPORT NO. NCSL 198-73
 CODE 0730R
- AUTH KEAR R.S.
 TITLE OILY WASTE DISPOSAL BY SOIL CULTIVATION PROCESS
 PUBL ENVIRONMENTAL PROTECTION TECHNOLOGY SERIES, DEC. 1972
 ABST THE PAPER DISCUSSES A STUDY DESIGNED TO DEMONSTRATE THE EFFECTIVENESS AND COST OF THE SOIL CULTIVATION PROCESS FOR DISPOSAL OF OILY WASTE FROM PETROLEUM.
 KEYW WASTE DISPOSAL, INDUSTRIAL WASTES TREATMENT, BIODEGRADATION
 CODE 0194R
- AUTH KETCHEL R.J., EDGERTON R.T.
 TITLE DEVELOPMENT OF USCG PROTOTYPE AIRBORNE OIL SURVEILLANCE SYSTEM
 PUBL DETECTION AND MONITORING OF SPILLS
 ABST DISCUSSION OF DEVELOPMENT, DESIGN AND FLIGHT TEST EVALUATION OF A PROTOTYPE AIRBORNE OIL SURVEILLANCE SYSTEM.
 KEYW DETECTION MAPPING, DOCUMENTATION
 CODE 0855F
- AUTH KHANDERRA R., SMITH T.S.
 TITLE APPLICATION OF THE CONCEPT OF BIPOLARIZED PLUME TO SOME OIL POLLUTION PROBLEMS IN THE STRAITS OF GAMBIA
 PUBL PROC. OF THE CANADIAN SOCIETY FOR CIVIL ENGR. FIRST CANADIAN HYD. CONF., 1973, ALBERTA UNIV. WATER RESOURCES CENTER, EDMONTON, 1973
 CODE 2036R
- AUTH KIMBLE R.E.

- TITLE** THE ESTIMATION OF IMPACT PRESSURES ARISING FROM THE IMPACT OF A DRUP AGAINST A SOLID SURFACE
PUBL ROYAL AIRCRAFT ESTABLISHMENT, LIBRARY TRANSLATION NO. 1054, AUG. 1972; PROCUREMENT EXECUTIVE RESEARCH REPORT
- ABST** IN THIS ESTIMATION OF IMPACT PRESSURES OF A DRUP WITH A SOLID SURFACE, THE DEFORMATION OF THE SURFACE OF THE DRUP AND THE ONSET OF POST-COLLISIONAL RITON OF THE LIQUID ARE CONSIDERED. IT IS ALSO SHOWN HOW EXCESSIVE PLATTENING OF THE DRUP LEADS TO A REDUCTION OF IMPACT PRESSURES.
- KEYW** IMPACT PRESSURES; DEFORMATION OF THE SURFACE OF THE DRUP; POST-COLLISIONAL RITON; EXCESSIVE PLATTENING
- CODE** 7074
- AUTH** KINARD V.S.
TITLE WASTE OIL RECOVERY AND DISPOSAL
PUBL POLLUTION TECHNOLOGY REVIEW NO. 20, NOV. DATA CORP., PARK RIDGE, N.J., 1973
- ABST** THE MAIN SUBJECTS OF WASTE OIL RECOVERY VERSUS NON POLLUTING DISPOSAL ARE OF HIGH CURRENT INTEREST BOTH FROM THE STANDPOINT OF CONSERVATION OF ENERGY RESOURCES AND THE PROTECTION OF THE ENVIRONMENT. RECOVERY, DISPOSAL, CONSERVATION AND PROTECTION.
- KEYW** RECOVERY, DISPOSAL, CONSERVATION AND PROTECTION
- CODE** 40114
- AUTH** KINNEY R.J., BUTTON D.R., SWEEL D.M.
TITLE KINETICS OF DISSIPATION AND BIODEGRADATION OF CRUDE OIL IN ALASKA COOK INLET
PUBL INSTITUTE OF MARINE SCIENCE, UNIVERSITY OF ALASKA, CONTRIBUTION NO. 61
- ABST** THE RESULTS OF A STUDY TO DEFINE THE MAGNITUDE OF OIL POLLUTION PROBLEMS IN ALASKA COOK INLET ARE REPORTED.
- KEYW** DISSIPATION; BIODEGRADATION RATES; ALASKA COOK INLET
- CODE** 21471
- AUTH** KIRKMAN R.L.
TITLE MODEL TEST OF A 1/2 SCALE OCEAN SYSTEM OIL RETENTION BARREL
PUBL TECH REPORT NO. 1046-1, OCEAN SYSTEMS, INC., 1970
- CODE** 07404
- AUTH** KITTREDGE J.S.
TITLE THE EFFECTS OF CRUDE OIL POLLUTION ON THE BEHAVIOR OF MARINE INVERTEBRATES
PUBL GOVERNMENT REPORT ANNOUNCEMENTS, 73(15):78
- CODE** 10348
- AUTH** KLEMAS V.
TITLE DETECTION AND MEASUREMENT OF OIL ON WATER
PUBL UNIV. OF DELAWARE
- ABST** DIFFERENCES IN PROPERTIES OF OIL AND WATER OFFERS A POTENTIAL METHOD FOR DETECTING POLLUTION. SUCCESSFUL DETECTION CAN DISCRIMINATE AMONG DIFFERENT OIL TYPES AND ARE NOT CONFUSED BY OTHER POLLUTANTS WHICH MAY RESIDE OIL.
- CODE** 18008
- AUTH** KLEMAS V., MAJALA D., LEATHAN B., KINNER P., TREASURE W.
TITLE ONE AND TWO-DIMENSIONAL STUDIES OF OIL DISPERSION AND OIL DISPERSION
PUBL JOURNAL OF WATER POLLUTION CONTROL FED. VOL. NO. 8, AUG. 1974
- ABST** THIS PAPER DISCUSSES THE RESEARCH OF A STUDY TO DETERMINE EFFECTS OF OIL SPILL AND OVER BOARD OIL DISPOSAL ON BENTHIC INVERTEBRATE COMMUNITIES.
- KEYW** SAMPLING; DISPERSION; DISPOSAL
- CODE** 21411
- AUTH** KLEMAS V., OLEY M., WELT L., RUTER B.
TITLE MONITORING COASTAL WATER PROPERTIES AND CURRENT CIRCULATION WITH ARTS-1, DELAWARE BAY
PUBL NASA, SCIENTS-1 SYM., VOL. 1, SECT. B, P1307-1411
- CODE** 04009
- AUTH** KNAPP R.
TITLE MICROBIAL DEGRADATION OF OIL: A REVIEW
PUBL ENVIRONMENTAL EMERGENCY BRANCH REPORT, REF. FROM 1975 CONF. ON PREVENTION AND CONTROL OF OIL POLLUTION
- CODE** 50248
- AUTH** KNAUSS J.A.
TITLE OCEAN POLLUTION: STATUS AND PROGNOSTICATION THE LAW OF THE SEA: THE EMERGING REGIME OF THE OCEANS, BULLINGER PUBLISHING CO., 1974
- ABST** KNAUSS DISCUSSES THE TIME-DEPENDENT NATURE OF OIL POLLUTION, EXPLAINS THE WAYS POLLUTANTS ENTER THE OCEAN, AND MAKES SOME PREDICTIONS AS TO THE FUTURE OF OIL POLLUTION.
- CODE** 31034
- AUTH** KNIGHT M.
TITLE INTERNATIONAL LEGAL PROBLEMS IN THE CONSTRUCTION AND OPERATION OF OFFSHORE DEEP DRAFT PUMP FACILITIES
PUBL THE HAZARDS OF MARITIME TRANSPORT, BULLINGER PUBLISHING CO., 1973
- ABST** THE PRINCIPLE OBJECTIVES OF THIS CHAPTER ARE TO IDENTIFY AND DISCUSS INTERNATIONAL LEGAL PRINCIPLES INVOLVED IN THE CONSTRUCTION AND OPERATION OF OFFSHORE DEEP DRAFT PUMP FACILITIES AND TO PROPOSE A DRAFT TREATY ARTICLE CONCERNING SUCH FACILITIES.
- CODE** 31034
- AUTH** KNOVEL F.
TITLE OIL AND WATER MIXTURES
PUBL OFFICE OF PUBLIC INFORMATION, NEW YORK, COLUMBIA UNIVERSITY
- ABST** THIS PAPER DISCUSSES THE RESULTS OF TESTS OF OIL AND WATER MIXTURES WITH THE HELP OF DISPERSANTS.
- KEYW** DISPERSANTS; MONOLAYER FILMS
- CODE** 21304
- AUTH** KOLMOGOROV, A.N.
TITLE THE BREAK-UP OF DROPLETS IN A TURBULENT STREAM
PUBL TRANSLATED FROM DOKL. AKADEM. NAUK. SO. SSSR
- ABST** STUDIES ON BREAK-UP IN A TURBULENT STREAM OF WATER DROPLETS OF LIQUIDS NOT SOLUBLE IN WATER.
- KEYW** TURBULENCE PULSATIUN; SIZE REDUCTIONS; PULSATIUN VELOCITIES
- CODE** 00341
- AUTH** KOLPAC R.
TITLE BEHAVIOR OF HYDROCARBONS FROM NATURAL SEEPS AND WELL BLOWOUT IN SANTA BARBARA CHANNEL CALIFORNIA
PUBL ABSTRACT VOLUME, SECOND NATIONAL COASTAL AND SHALLOW WATER RESEARCH CONFERENCE
- ABST** THIS REPORT DISCUSSES THE PHYSICAL AND CHEMICAL INFORMATION OBTAINED TO PROVIDE QUANTITATIVE METHODS OF DETERMINING THE BEHAVIOR OF SPILLED OIL.
- KEYW** DISTRIBUTION; DISSOLUTION; OIL SEEPS
- CODE** 20351
- AUTH** KOLPAC R.
TITLE PRIORITIES IN FATE OF OIL SPILL RESEARCH
PUBL 1977 OIL SPILL CONFERENCE
- ABST** RESEARCH EFFORTS THAT WILL BE REQUIRED TO GAIN A BETTER UNDERSTANDING OF THE FATE OF OIL IN THE OCEAN ARE CATEGORIZED WITH RESPECT TO FIVE MAJOR ENVIRONMENTAL MECHANISMS.
- KEYW** INTERACTION; MARINE ENVIRONMENT; SPREADING; MIXING; DISSOLUTION; EMULSIFICATION; DEGRADATION
- CODE** 12341
- AUTH** KOLPAC R.J., RECHMANS B.J., MYERS J.J., PLUTCHAK R.B., EATON E.
TITLE FATE OF OIL IN A WATER ENVIRONMENT, PHASE I, VOL. 1
PUBL ENVIRONMENTAL GEOLOGY PROGRAM, API PUBLICATION, NO. 4212
- ABST** THIS REPORT PRESENTS THE RESULTS OF AN EVALUATION OF THE LITERATURE TO DETERMINE WHAT IS KNOWN ABOUT THE FATE OF OIL RELEASED TO THE WATER ENVIRONMENT. MASS BALANCE RELATIONSHIPS, OIL SPREAD.
- KEYW** MASS BALANCE RELATIONSHIPS; OIL SPREAD
- CODE** 25421
- AUTH** KOLPAC R.J.
TITLE FATE OF OIL IN A WATER ENVIRONMENT - PHASE II: A DYNAMIC MODEL OF THE MASS BALANCE FOR RELEASED OIL, FINAL REPORT, MARCH 1977
PUBL DEPARTMENT OF ENVIRONMENTAL AFFAIRS, AMERICAN PETROLEUM INSTITUTE
- ABST** A THREE-DIMENSIONAL DIGITAL COMPUTER SIMULATION MODEL WAS CONSTRUCTED FOR THE PURPOSE OF ORGANIZING THE AVAILABLE INFORMATION FROM OIL SPILL RESEARCH EFFORTS IN ORDER TO DEVELOP A MANAGEMENT & SCIENTIFIC TOOL WHICH COULD BE USED TO GAIN A BETTER UNDERSTANDING OF THE FATE OF OIL RELEASED IN ICE FREE MARINE ENVIRONMENTS. RESULTS SHOW THAT THE FATE OF A PARTICULAR OIL SPILL DEPENDS ON A COMBINATION OF FACTORS SUCH AS TYPE OF OIL INVOLVED, VOLUME RELEASED, RESIDENCE TIME IN A GIVEN AREA, & ENVIRONMENTAL CONDITIONS AT THE SITE OF THE SPILL.
- KEYW** THREE-DIMENSIONAL MODEL; OIL SPILL RESEARCH
- CODE** 17031
- AUTH** KOLPAC R., PLUTCHAK R.
TITLE ELEMENTS OF MASS BALANCE RELATIONSHIPS FOR OIL RELEASED IN THE MARINE ENVIRONMENT
PUBL ENVIRONMENTAL GEOLOGY, UNIV. OF SO. CALIFORNIA
- ABST** THE COMPOSITION OF OIL RELEASED IN THE MARINE ENVIRONMENT AND THE PROCESS AND PARAMETERS WHICH INFLUENCE THE COMPOSITION, QUANTITY AND SPATIAL DISTRIBUTION OF HYDROCARBONS IN THE ENVIRONMENT ARE THE CONTROLLING FACTOR IN DETERMINING THE FATE OF AN OIL SPILL.
- KEYW** COMPOSITION; QUANTITY; SPATIAL DISTRIBUTION; FATE
- CODE** 20341
- AUTH** KOLPAC R.L.
TITLE MOVEMENT OF OIL AND WATER IN SANTA BARBARA CHANNEL, CALIFORNIA
PUBL UNIV. OF CALIF., FOR 1969 JOINT CONFERENCE
- KEYW** MOVEMENT; SANTA BARBARA CHANNEL
- CODE** 02031
- AUTH** KORDA G.
TITLE ABOUT THE PROPERTY OF DISPERSING METHOD FOR SPILLED OIL
PUBL PAPER PRESENTED AT THE SECOND INTERNATIONAL OCEAN DEVELOPMENT CONFERENCE, OCT. 1972
- CODE** 10274
- AUTH** KODINS C.B., MCMALEFFE C.O., WEISS F.T.

- TITLE ENVIRONMENTAL ASPECTS OF PRODUCED WATERS FROM OIL AND GAS EXPLORATION OPERATIONS IN OFFSHORE AND COASTAL WATERS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2447, MAY 2-6, 1976
 ABST THIS PAPER REVIEWS THE CONSTITUENTS OF PRODUCED WATERS AND THEIR EFFECTS ON BOTH OFFSHORE AND COASTAL MARINE ENVIRONMENTS. INTERPRETATION OF CONSIDERABLE LABORATORY AND FIELD DATA WITH CONCLUSIONS.
 REYO TOXICITY, DILUTION, EVAPORATION, FIELD DATA
 CODE 26231
- AUTH ROZDORAN E., CUREN S.
 TITLE A METHOD FOR MEASURING OIL THICKNESS ON THE SURFACE OF WATER IN THE PRESENCE OF WAVES, CAVITATION AND POLYPHASE FLOW FUROR, 1977
 PUBL THIS PAPER DISCUSSES THE NEED TO UNDERSTAND THE BEHAVIOR OF OIL ON WATER TO DESIGN AN EFFECTIVE RECOVERY DEVICE.
 REYO OIL THICKNESS, CONTAINMENT, CLEANUP, RECOVERY
 CODE 65021
- AUTH BOWALSKI A.
 TITLE LIGHTWEIGHT OIL CONTAINMENT BARRIER FIELD TESTS
 PUBL US NAVAL CIVIL ENG. LAB., SO EPA 670/2-75-003
 CODE 2008-
- AUTH REEDS C.T., BURNS A.A.
 TITLE LONG TERM EFFECTS OF AN OIL SPILL ON POPULATIONS OF THE SALT MARSH CRAB
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST DISCUSSION OF RESULTS OF LONG TERM EFFECTS OF OIL ON SALT MARSH CRABS.
 REYO CRAB POPULATIONS, SALT MARSHES, LONG TERM EFFECTS
 CODE 20091
- AUTH KRUMP F., MALDUNSEN J., ODUNDSON T.
 TITLE OILSIM - A COMPUTER PROGRAM SIMULATING THE FATE OF OIL SPILLS
 PUBL NORTH OCEANIC MARITIME RESEARCH NO. 4/1978 REPRIAT
 ABST THIS PAPER PRESENTS A COMPUTER MODEL, OILSIM, FOR THE SIMULATION OF THE DRIFT, SPREADING, DISSIPATION AND WEATHERING OF OIL SPILLS. THE OILSIM COMPUTATIONS ARE BASED ON A SIMPLE ONE-DIMENSIONAL BUOYANT MODEL.
 REYO OILSIM, OIL SPILLS, WEATHERING
 CODE 77431
- AUTH NUTT E.C., MARTIN D.F.
 TITLE EFFECT OF SELECTED SURFACTANTS ON THE GAUßIN CHARACTERISTICS OF CYMMODINIUM BREVIE
 PUBL MAR. BIL. 26:253-254
 CODE 1013P
- AUTH KUMRITSKY G.A., PANIN L.N.
 TITLE EFFECT OF AN OIL SLICK ON THE SEA SURFACE ON TURBULENCE AND THE LAYER OF THE ATMOSPHERE NEAR TO THE WATER
 PUBL METEOROLOGICAL AND HYDROLOGY
 CODE 0304P
- AUTH LA ROCA P.A., AMFIELD J.E.
 TITLE THE RELATIVE CHANGES IN N-ALKANE COMPOSITION IN SURFACE WATER SLICKS
 PUBL LOUISIANA STATE UNIV. SEA GRANT PUBLICATION NO. LSU-SG-73-01
 CODE 0324P
- AUTH LACAZE J.
 TITLE INFLUENCE OF THE ILLUMINATION OF A NON-IONIC SURFACTANT USED FOR THE DISPERSION OF OIL SPILLS AT SEA
 PUBL EPA, PD-237805-1, JULY 28, 1973
 ABST THE INFLUENCE OF THE ILLUMINATION IS USUALLY NEGLECTED IN THE ASSAYS OF BIODEGRADATION. IT IS THIS PARAMETER THAT WE STUDY IN THIS PAPER AND ITS ACTION ON THE BIODEGRADATION OF A NON-IONIC SURFACTANT.
 REYO BIODEGRADATION, TANKER SHIPS, SURFACTANTS, PETROLEUM INDUSTRY
 CODE 5100F
- AUTH LAFOND E.C., LAFOND E.C.
 TITLE SEA SURFACE SLICKS
 PUBL PAUL. NAVAL UNDERSEA RESEARCH AND DEVELOPMENT CENTER, MARCH 1971, REPORT NO. NUC TP 215
 CODE 2037H
- AUTH LAIR M.C., ROGERS A.C., MELDON M.R.
 TITLE ENVIRONMENTAL EFFECTS OF PETROCHEMICAL WASTE DISCHARGES ON TALLADGA AND GUANTANILLA BAYS, PUERTO RICO
 PUBL EPA, REGION IV, SURVEILLANCE AND ANALYSIS DIV., OCT. 1971
 ABST OBJECTS OF REPORT: 1. CHARACTERIZE AND QUANTIFY WASTES, 2. DETERMINE THE EFFECTS OF THESE WASTES, 3. DOCUMENT VIOLATIONS OF PUERTO RICO'S FEDERAL STATE COASTAL WATER QUALITY STANDARDS.
 REYO CHARACTERIZE, QUANTIFY, EFFECTS, WASTES, VIOLATIONS, FEDERAL, STATE, STANDARDS
 CODE 0031A
- AUTH LALLIER B.
 TITLE CHANGES IN THE DIFFERENTIATION OF THE SEA MICHIA LARVA BY ACTION OF A DETERGENT UPON THE
- UNSEGMENTED ECC
 PUBL EXPERIENTIA 29/6, SPECIALIA
 ABST THIS PAPER DISCUSSES THE EFFECTS OF CHEMICAL DISPERSANTS ON THE SEA MICHIA LARVA.
 REYO SEA MICHIA LARVA, DISPERSANTS, DIFFERENTIATION
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- AUTH LAM D.
 TITLE AN ELECTRO-ACOUSTIC OIL LAYER THICKNESS GAUGE
 PUBL UMI THESIS 1975
 ABST THIS PAPER DESCRIBES THE CONSTRUCTION AND TESTING OF A SUCCESSFUL ELECTRO-ACOUSTIC OIL LAYER THICKNESS GAUGE
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- AUTH LANGMUIR J.
 TITLE SURFACE MOTION OF WATER INFLUENCED BY WIND
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 ABST THIS PAPER DISCUSSES THE EFFECT OF WIND ACTION ON WAVES.
 REYO LONGITUDINAL SURFACE CURRENTS, HELICAL VORTICES, WIND DIRECTION
 CODE 2654F
- AUTH LARUCHE G., ELSNER A., TARIWELL C.
 TITLE BEGASSAY PROCEDURES FOR OIL AND GIL DISPERSANT TOXICITY EVALUATION
 PUBL JOURNAL OF WATER POLLUTION CONTROL, VOL. 42, NOV. 1973
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 CODE 2143F
- AUTH LARRABEE R.M., BROWN G.A.
 TITLE AN IN-SITU INVESTIGATION OF OIL BARRIER SHAPE AND DRAG COEFFICIENTS
 PUBL UMI DEPT. OF C.E., MAY 1974
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 REYO CODE 4029B
- AUTH LARSON J.J.
 TITLE AN EXAMINATION OF ALTERNATIVE METHODS FOR EMPLOYING BORDS TO CONTAIN OIL SPILLS IN NAVY HARBORS
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 REYO CODE 6104A
- AUTH LASKIN A., LECHEVALIER P.
 TITLE CRITICAL REVIEWS IN MICROBIOLOGY
 PUBL CRITICAL REVIEW JOURNAL
 ABST VARIOUS ARTICLES PERTAINING TO MICROBIOLOGY.
 CODE 7200F
- AUTH LATIFF S.A.
 TITLE THE EFFECT OF OIL SLICK DISPERSANT ESSO CORALITE 7000 AND THE JOINT EFFECT WITH CALUM OIL ON THE SURVIVAL OF MARINE GLASS PISH ANNESSIS AND PALLERONIC SWIMMY
 PUBL MALAY AGRIC. J., 48:12-19, 1971
 CODE 1017H
- AUTH LAU Y.C., KIRCHMEYER S.A.
 TITLE A REVIEW OF THE DYNAMICS OF CONTAINED OIL SLICKS IN FLEETING WATER
 PUBL HYDRAULICS DIVISION INLAND WATER DIRECTORATE, OIL, 1974, REPORT NO. EPS-2-1974-3
 ABST A REVIEW OF PUBLISHED PAPERS DEALING WITH THE DYNAMICS OF CONTAINED OIL SLICKS IN FLEETING WATER HAS BEEN MADE.
 REYO ONE-DIMENSIONAL FLOWS, CONTINUITY AND RECOVERY, THICKNESS
 CODE 7142F
- AUTH LAHLER G.C., MEN-AN L.
 TITLE ACCUMULATION OF SAHARATED HYDROCARBONS IN TISSUES OF PETROLEUM-EXPOSED MALLARD DUCKS (ANAS PLATYRHYNCHOS)
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 REYO MALLARD DUCKS, PETROLEUM HYDROCARBONS, GAS CHROMATOGRAPHY, MASS SPECTROMETRY
 CODE 7707 F
- AUTH LAHLER G.C., MEN-AN L., LARSEN J.L.
 TITLE ACCUMULATION OF AROMATIC HYDROCARBONS IN TISSUES OF PETROLEUM EXPOSED MALLARD DUCKS (ANAS PLATYRHYNCHOS)

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- ABST WALLARD DRINKS WERE OUSED WITH 5 ML A DAY OF SOUTH
LOUISIANA CRUDE OIL FOR FOURTEEN DAYS. TISSUES
FROM CONTAINMENT AND OIL DOSED DUCKS WERE EXAMINED FOR
AROMATIC PETROLEUM HYDROCARBONS BY COMBINED
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- CODE 7708 F
- AUTH LE BLANC L.
TITL BARRIER LOAD TESTS IN THE ARCTIC
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- AUTH LEARY J.P.
TITL HIGH SEAS OIL RECOVERY SYSTEMS DEVELOPMENT AND
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- ABST THIS PAPER DISCUSSES THE DEVELOPMENT OF A RECOVERY
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- KEYS RECOVERY, FREE VORTICES, NEAR-BASIN, DISC-DRUM
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- AUTH LEE C.Y., RASCH P.
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- ABST THIS REPORT INVOLVES A LAB. STUDY OF THE
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THE PURPOSE OF THE INVESTIGATION IS TO ELUCIDATE THE
NATURE OF WIND WAVE INDUCED TURBULENCE IN ORDER TO
OBTAIN A BETTER UNDERSTANDING OF ITS ROLE IN THE
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- CODE 2925R
- AUTH LEE R.F.
TITL PALE OF PETROLEUM HYDROCARBONS IN MARINE
ZOOPLANKTON
PUBL SAIDABAT INSTITUTE OF OCEANOGRAPHY, FOR EPA 1975
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- KEYS PALE, HYDROCARBONS, MARINE ZOOPLANKTON
CODE 0147R
- AUTH LEE R.F., GARDNER D.S.
TITL PALE OF POLYCYCLIC AROMATIC HYDROCARBONS IN
CONTROLLED ECOSYSTEM ENCLOSURES
PUBL ENVIRONMENTAL SCIENCE & TECHNOLOGY VOLUME 12,
NUMBER 7, JULY 1978
- ABST PRUDHOPE CRUDE OIL ENRICHED WITH A NUMBER OF
POLYCYCLIC AROMATIC HYDROCARBONS WAS ADDED AS A
DISPERSION TO A CONTROLLING ECOSYSTEM ENCLOSURE
SUSPENDED IN SAGINAW INLET, CANADA.
CONCENTRATIONS OF VARIOUS AROMATICS WERE
DETERMINED IN WATER, ZOOPLANKTON, SYSTEMS AND
BOTTOM SEDIMENTS. THIS PAPER SUMMARIZES AN
EXPERIMENTAL STUDY OF THE FATE OF A NUMBER OF
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- AUTH LEE R.F., SAVERIMORE A., WOODS D.M.
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- AUTH LEE W.T.
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- ABST THIS PAPER DISCUSSES THE IMPORTANCE OF THE
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- AUTH LEENGWATSE J.J.
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- AUTH LEHR W.E.
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- AUTH LEHR W.E., SCHREIER J.
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- ABST THE GENERAL REQUIREMENTS FOR HIGH SEAS OIL SPILL
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0817F
- AUTH LEIBOVICH S.
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- ABST THE THEORETICAL PERFORMANCE OF OIL SPILL CONTROL
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- AUTH LEIBOVICH S.
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- ABST A SIMPLE STATISTICAL MODEL IS DEVELOPED TO
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- KEYS VERTICAL TURBULENT TRANSPORT, OIL SPILL
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- AUTH LEIBOVICH S.
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- ABST EXPERIMENTAL EVIDENCE SHOWING OIL SLICK
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- AUTH LEITON J.T.
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- KEYS RECOVERY, ALTATING DISCORDUM, WAVE COMPRESSING
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- AUTH LERENHAUTE B.
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- AUTH LEONARD R.L.
TITL RESULTS PRODUCED BY A TECHNOLOGY ASSESSMENT OF OIL
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- AUTH LEITTA J., WALLACE W.A.
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- KEYS INCIDENT REPORTING SYSTEM, PROGRAM MANAGEMENT,
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- AUTH LEPPAKOSKI E.J., LINGSTROM L.S.
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- AUTH LESHT B.J., WHITE R.V., MILLER R.L.
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- ABST THIS REPORT DESCRIBES THE DESIGN, OPERATION,
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- AUTH LEWIS E.V.
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 ABST THIS PAPER SUMMARIZES TECHNIQUES THAT MAY BE
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 KEYW WIND-WAVES, TURBULENCE, DISPERSION, BREAKING WAVES
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AUTH LINDEN G.
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AUTH LINDENMUTH W.T.
 TITLE ANALYSIS AND MODEL TESTS TO DETERMINE FORCES AND
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 KEYW PHYSICAL PROPERTIES, HYDRODYNAMIC PROPERTIES,
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 CODE 0540F

AUTH LINDENMUTH W.T.
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AUTH LINDENMUTH W.T., MILLER E.R., HSL C.C.
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 KEYW CONTAINMENT, OIL BOOMS, HYDRODYNAMICS
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 KEYW BOOMS, SAMPLERS, CONTROL

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AUTH LINDENMUTH, SCHWEN, VAN DYKE
 TITLE NO. 4 - NO. 13
 PUBL HYDROAUTICS INC.
 ABST GRAPHS INCLUDING OIL BOOM MODEL TEST DRAW, DRAG
 COEFFICIENT VERSUS OCCURANCE RATION, WAVE
 COEFFICIENT VERSUS RELATIVE OIL DEPTH.
 CODE 0020F

AUTH LISSAUER I.
 TITLE A TECHNIQUE FOR PREDICTING THE MOVEMENT OF OIL
 SPILLS IN NEW YORK HARBOR
 PUBL DEPT. OF TRANSPORTATION, USCG
 ABST THROUGH EXPERIMENTS WHICH WERE CONDUCTED IT IS
 APPARENT THAT THE MAJOR FACTORS INVOLVED IN THE
 TRANSPORT OF AN OIL SLICK IN NEW YORK HARBOR ARE
 WINDS, TIDES AND FRESH WATER FLOW FROM THE HUDSON
 RIVER.
 KEYW WINDS, TIDES, FLOWS, TRANSPORT OF AN OIL SLICK
 CODE 2575A H

AUTH LISSAUER I., BACON J.
 TITLE FINAL REPORT, PREDICTED OIL SLICK MOVEMENT FROM
 VARIOUS LOCATIONS OFF THE NEW JERSEY - DELAWARE
 COASTLINE
 PUBL USCG, DEPT. OF TRANSPORTATION, CGA-DC 13/75, JUNE
 1975
 ABST AVERAGE MONTHLY WIND SPEEDS AND DIRECTIONS AND
 MONTHLY CURRENT PATTERNS WERE USED FOR PREDICTING
 THE OIL SLICK MOVEMENT. PROBABLE AREAS OF IMPACT
 ALONG THE SHORELINE WERE INDICATED.
 KEYW OIL SLICK MOVEMENT, PREDICTING MOVEMENT, CURRENT
 PATTERNS
 CODE 2540F

AUTH LISSAUER I.M.
 TITLE FINAL REPORT, A TECHNIQUE FOR PREDICTING THE
 MOVEMENT OF OIL SPILLS IN NEW YORK HARBOR
 PUBL USCG, DEPT. OF TRANSPORTATION, CG-U-0-75, FEB.
 1974
 ABST THIS PAPER DISCUSSES THE MAJOR FACTORS INVOLVED IN
 THE TRANSPORT OF AN OIL SLICK.
 KEYW OIL TRANSPORT, SPILL FORECASTING, SPILL MONITORING
 CODE 2581F

AUTH LISSAUER I.M., WELSH J.P.
 TITLE FINAL REPORT, PRELIMINARY PREDICTIONS OF OIL SPILL
 MOVEMENT FOR THREE POTENTIAL DEEP WATER PORT SITES
 IN THE GULF OF MEXICO
 PUBL USCG, DEPT. OF TRANSPORTATION, CGA AND DC 34/75,
 DEC. 1975
 ABST PREDICTIONS OF THE MOVEMENT OF OIL SLICKS AND
 THEIR IMPACT LOCATION ALONG THE SHORELINES OF
 TEXAS, LOUISIANA, MISSISSIPPI, ALABAMA AND FLORIDA
 WERE DETERMINED FROM THREE POTENTIAL DEEP WATER
 PORT SITES. AVERAGE MONTHLY WIND SPEEDS,
 DIRECTIONS AND CURRENT PATTERNS WERE USED IN
 PREDICTING OIL SLICK MOVEMENT.
 KEYW OIL SLICK MOVEMENT, PREDICTING, DEEPWATER PORTS,
 WIND DRIFT
 CODE 2547F

AUTH LISU D.L., DUTKA B.T.
 TITLE BIOLOGICAL OXIDATION OF HYDROCARBONS AQUEOUS PHASE
 PUBL JOURNAL WPLE, VOL. 95, NO. 2, FEB. 1973
 CODE 1100R

AUTH LODGE T.C.
 TITLE AUTOANALYZER METHODOLOGY AND ITS ROLE IN ESTUARINE
 AND OCEANIC ECOSYSTEM MODELING
 PUBL UNIVERSITY OF NEW HAMPSHIRE, DUMFRIES 03824
 DEPARTMENT OF EARTH SCIENCES WITH TECHNICAL
 INTERNATIONAL SYMPOSIUM ON ENVIRONMENTAL CHANGES
 AND BIOLOGICAL RESPONSE, TOKYO JAPAN 1970
 ABST THE AUTOANALYZER PROVIDES THE MEANS FOR ANALYZING
 THE LARGE NUMBER OF SAMPLES REQUIRED IN MODELING
 RESEARCH. SPECIAL PRECAUTIONS MUST BE UTILIZED IN
 THE ANALYSIS OF THESE WATERS; MULTIVARIABLE
 CHEMICAL NATURE AFFECTING THE ACCURACY OF THE
 ANALYSES. METHODS FOR DETERMINING THESE
 CORRECTIONS WITHOUT USING ARTIFICIAL SEA WATER ARE
 PRESENTED.
 KEYW ESTUARIES, NUTRIENTS, MODELS, OCEANOGRAPHIC DATA.
 CODE 7704 F

AUTH LOFTAS T.
 TITLE THE UNSURE DANGERS OF OIL
 PUBL NEW SCIENTIST AND SCIENCE JOURNAL, 65(737):220,
 FEB. 20 1971
 CODE 1110R

AUTH LOGAN J.W.R.
 TITLE OIL DISPERSANT TOXICITY
 PUBL MARINE POLLUTION BULL. 0667190-03
 CODE 1070F

AUTH LOGAN W., THORNTON D., BOSS D.L.
 TITLE OIL SPILL COUNTERMEASURES FOR THE SOUTHERN
 BEAUFORT SEA - APPENDIX
 PUBL BEAUFORT SEA PROJECT, TECH. REPORT NO. 310, DEPT.
 OF THE ENVIRONMENT
 ABST THIS REPORT DISCUSSES THE FEASIBILITIES OF
 CONTROLLING AND CLEANING UP AN OIL SPILL IN THE
 BEAUFORT SEA AS A RESULT OF AN EXPLOSIONARY WELL
 BLOWOUT.

AUTH BLOMQUIST, CONTROL, CLEANUP
 CODE 71007
 AUTH LOGAN W.J.
 TITLE OIL SPILL COUNTERMEASURES FOR THE BEAUFORT SEA
 PUBL CENTRAL OF SPILL TECHNOLOGY, EPA, COMPREHENSIVE 1975
 ABST PAPER INCLUDES: THE BEAUFORT SEA PROJECT, GIL IN ICE STUDIES, COUNTERMEASURE STUDIES, AND PROGRESS MADE UP UNTIL DEC. 1974.
 REYO BEAUFORT SEA, GIL IN ICE, COUNTERMEASURES, PROGRESS
 CODE 01004
 AUTH LOGAN W.J., THORNTON D.E., ROSS S.L.
 TITLE OIL SPILL COUNTERMEASURES OF THE SOUTHERN BEAUFORT SEA
 PUBL BEAUFORT SEA TECHNICAL REPORT NO. 31A
 ABST THIS REPORT DISCUSSES THE FEASIBILITIES OF CONTROLLING AND CLEANING UP AN OIL SPILL IN THE BEAUFORT SEA AS A RESULT OF AN EMERGENCY WELLS BLOW-OUT.
 REYO BLOW-OUT, CONTROL, CLEANUP
 CODE 71007
 AUTH LONGUET-MIGGINS M.S.
 TITLE MASS TRANSPORT IN THE BOUNDARY LAYER AT A FREE OSCILLATING SURFACE
 PUBL NATIONAL INSTITUTE OF OCEANOGRAPHY, NOV. 1955
 ABST THIS PAPER DESCRIBES LABORATORY EXPERIMENTS WHICH CONFIRM THE HIGHER VALUE OF THE GRADIENT.
 REYO BOUNDARY LAYER, MASS-TRANSPORT GRADIENT, INSTATIONARY THEORY, OSCILLATORY BOUNDARY LAYER
 CODE 91227
 AUTH LOU T.
 TITLE A STUDY OF THE EFFECTS OF RAINDROPS ON OIL FILMS
 PUBL SUBMITTED BY THOMAS LOU AS A PARTIAL FULFILLMENT OF UCI 852
 ABST SPECIAL PROBLEM STUDY OF OIL/WATER MIXING PROCESSES.
 REYO RAINDROPS, OIL/WATER MIXING, INTERFACE PENETRATION
 CODE 03157
 AUTH LOUCAS R.M.
 TITLE DISPERSION OF SPILLED OIL
 PUBL FISHERIES RESOURCE BOARD OF CANADA, TECH. REPORT NO. 420, 1974
 CODE 20207
 AUTH LOUCAS R.M., LAWRENCE D.J., INGHAM D.V.
 TITLE MODEL ON ESTIMATION OF PLUME AND PATCH DISPERSION SCALES
 PUBL APPLIED STATISTICS, PROCEEDINGS OF THE CONFERENCE AT QUEBEC, QUEBEC, MONTREAL, MAY 2-6, 1974
 ABST THE PURPOSE OF THIS MODEL IS TO DESCRIBE A GENERALIZED TECHNIQUE FOR ESTIMATING PLUME DISPERSION FROM OCEAN CURRENT AFTER TIME SERIES DATA.
 REYO PLUME DISPERSION, OCEAN CURRENT RETURN, RANGE ANALYSIS
 CODE 71157
 AUTH LUO B.C., PLEEN J.
 TITLE A STUDY OF THE SOLUBILITY OF OIL IN WATER
 PUBL TECHNOLOGY DEVELOPMENT REPORT, NO. EP5-70-1-70-1, ENVIRONMENTAL CONSERVATION DIRECTORATE, FEB. 1974
 ABST EXPERIMENTS WERE CONDUCTED TO DETERMINE THE IC50 SOLUBILITY OF OIL IN WATER. THREE OILS WERE EMPLOYED: NO. 2 FUEL OIL, MEDIUM BURNER FUEL AND WESTERN CRUEL.
 REYO DISPERSION, HYDROCARBONS, SOLUBILITY
 CODE 71007
 AUTH LUMENS M.R.
 TITLE OIL SLICK IDENTIFICATION
 PUBL PREPARED BY GUP RADIATION TECH., CONTRACT NO. AT(50)-31-127
 ABST INSTRUCTION MANUAL FOR OIL SLICK IDENTIFICATION BY TRACE ELEMENT PATTERNS MEASURED WITH NEUTRON ACTIVATION ANALYSIS.
 CODE 00004
 AUTH LUTNEY B., RUBERT C., SELLECK E., GALLAGHER J.P.
 TITLE SURFACE PROPERTIES OF PETROLEUM REFINERY WASTE OIL EMULSIONS
 PUBL UNKNOWN
 ABST THE SURFACE PROPERTIES OF OIL EMULSIONS IN REFINERY WASTEWATER WERE FOUND TO BE DETERMINED LARGELY BY WATER QUALITY RATHER THAN BY SOURCE OF OIL.
 REYO SURFACE PROPERTIES, OIL EMULSIONS, REFINERY WASTEWATER, WATER QUALITY
 CODE 70027
 AUTH LYNCH P.F.
 TITLE THE WEATHERING AND SUBSEQUENT SOURCE IDENTIFICATIONS OF OIL SPILLS USING INFRARED SPECTROSCOPY
 PUBL 1973
 ABST THIS MASTER'S THESIS DISCUSSES HOW INFRARED SPECTROSCOPY ALONG WITH THE USE OF A COMPUTER PROGRAM PROVIDES A MEANS OF CATALOGING AND/OR PETROLEUM SAMPLES AND HAS MADE IT POSSIBLE TO MATCH AN OIL SPILL TO ITS SOURCE UP TO 30 DAYS AFTER THE ORIGINAL SPILL.
 CODE 30034
 AUTH LYNCH P.F., BRADY M.C.
 TITLE COMPUTERIZED INFRARED SPECTROSCOPY AS A SEPARATION

TECHNIQUE-ANALYSIS OF COMPLEX ORGANIC MIXTURES EXTRACTED FROM WATER
 PUBL INT. DEPT. OF CHEMISTRY
 ABST A METHOD FOR DETERMINATION OF COMPLEX INSTRUMENTAL CONDITIONS FOR COLLECTION OF ACCURATE DISPERSIVE INFRARED DATA HAS BEEN OBTAINED AND SUCCESSFULLY USED ON SEVERAL COMPLEX ORGANIC MIXTURES.
 REYO INSTRUMENTAL CONDITIONS, DISPERSIVE INFRARED DATA, COMPLEX ORGANIC MIXTURES
 CODE 70007
 AUTH LYSTA J., RUSSELL E.L.
 TITLE DISSOLUTION OF PETROLEUM DERIVED PRODUCTS IN WATER
 PUBL WATER RESEARCH, VOL. 1, 1974
 CODE 20007
 AUTH LYTEL J.S.
 TITLE PALEO AND EFFECTS OF CRUDE OIL ON AN ESTUARINE PLANT
 PUBL WULF COAST RESEARCH LAB. FOR EPA 1975 CONFERENCE
 REYO PALEO AND EFFECTS, CRUDE OIL, ESTUARINE PLANT
 CODE 01507
 AUTH MBLINTYNE W.G., SMITH G.L., RUMPT J.L., GIBSON W.R., LARK J.L.
 TITLE INVESTIGATION OF SURFACE FILMS - CHESAPEAKE BAY AREA
 PUBL EPA - TECHNOLOGY SERIES REPORT, EPA 870/2-73-004
 CODE 03017
 AUTH MELBY U., LEINOHEN P.V.
 TITLE MATHEMATICAL MODEL OF THE BEHAVIOR OF OIL SPILLS ON WATER WITH NATURAL AND CHEMICAL DISPERSIBLE FISHES AND ENVIRONMENT - CANADA, EP5
 PUBL 8-11-77-15, OCT. 1977
 ABST A MATHEMATICAL MODEL OF THE BEHAVIOR OF AN OIL SPILL ON WATER HAS BEEN ASSEMBLED AND SOLVED IN A DIGITAL COMPUTER TO YIELD DATA ON THE SPILL SLICK SIZE, THICKNESS, PROPERTIES, AND COMPOSITION, ON THE AMOUNTS OF OIL EVAPORATED, DISSOLVED AND DISPERSED; AND ON THE CONCENTRATION HISTORY OF THE HYDROCARBON DISSOLVED IN THE WATER COLUMN.
 REYO MATHEMATICAL MODEL, DIGITAL COMPUTER, SLICK THICKNESS, PROPERTIES, COMPOSITION
 CODE 70207
 AUTH MELBY U., BOLDOFF A.W.
 TITLE RATE OF EVAPORATION OF LOW SOLUBILITY CONTAMINANTS FROM WATER BODIES TO ATMOSPHERE
 PUBL ENVIRONMENTAL SCIENCE AND TECH. VOL 7, 1973
 CODE 20027
 AUTH MERRAT G.D.
 TITLE STABILITY OF BUNKER C SEAWATER EMULSION
 PUBL DEPT. OF CHEM. ENGR., NOVA SCOTIA TECH. COLLEGE, 1970
 CODE 20037
 AUTH MERRAT G.D.
 TITLE AVOIDANCE REACTIONS OF MARINE INVESTITED TO EARTH BENTHIC CYCLOPOIDS OF STATION ON SYNTHETIC SURFACE-ACTIVE AGENT.
 PUBL J. EAP. MAR. BIOL. OCEAN., 5:103-109, 1970
 CODE 20107
 AUTH MERRAT P.R., HARDY R., WHITTLE R.J.
 TITLE PRELIMINARY ASSESSMENT OF THE PRESENCE OF OIL IN THE ECOSYSTEM AT BAUFISK AFTER THE OILWEL AFTER 22-JULY 1977
 PUBL JOURNAL OF THE FISHERIES, VOL. 33, NO. 5, MAY 1970
 ABST THE MARINE ENVIRONMENT IN THE FISHING AREA WAS ASSESSED FOR THE PRESENCE OF OIL COMPONENTS AFTER THE OILWEL ON PLATFORM BRAND WAS OBTAINED UNDER CONTROL. SEVERAL METHODS OF ASSAY WERE USED BUT THE RESULTS WERE NOT ALWAYS STRICTLY COMPARABLE.
 REYO FISHING, SURFACE FILM, SEDIMENT
 CODE 20007
 AUTH MERRIN G.S.
 TITLE A REALISTIC MODEL OF THE WIND-INDUCED EMANATION BOUNDARY LAYER
 PUBL BOUNDARY LAYER JOURNAL OF PHYSICAL OCEANOGRAPHY, MARCH 1977
 ABST A PHYSICALLY REALISTIC AND GENERAL MODEL FOR THE VERTICAL BOUNDARY REALITY IN A HOMOGENEOUS FLUID IS PROPOSED. THE APPLICATION OF THE MODEL TO FINE-SCALE DEPTH CONDITIONS, INCLUDING THE EFFECTS OF SLOPE CURRENTS, IS OUTLINED.
 REYO VISCOSITY, EMAN BOUNDARY
 CODE 77007
 AUTH MERTZ E.
 TITLE EVAPORATION OF OIL FROM SLICKS
 PUBL PROC. OF A CONF. ON OIL AND THE CANADIAN ENVIRONMENT, UNIV. OF TORONTO, MAY 1973
 CODE 20057
 AUTH MERRIVILLE C.R.
 TITLE STATE-OF-THE-ART REVIEW OF OIL CONTAINMENT BARRIERS FOR USE AT OFFSHORE TERMINALS
 PUBL REPORT MARAL-272-23100-01, US NAT. MARITIME RES. CENTER
 CODE 07357
 AUTH MERRISAI J.J., OBIEN E.B., REYNOLDS M.
 TITLE KINETIC STUDY OF A FUEL OIL UNDERGOING PHOTO-CHEMICAL WEATHERING

- PUBL ENVIRONMENTAL LETTERS
REFV SCIENTIFIC STUDY, PHOTOCHEMICAL WEATHERING
CODE 0301R
- AUTH HALINS D.C.
TITL EFFECTS OF PETROLEUM ON ARCTIC AND SUBARCTIC MARINE ENVIRONMENT AND ORGANISMS VOLUME I NATURE AND FATE OF PETROLEUM
PUBL ACADEMIC PRESS INC.
ABST VOLUME I DEALS WITH THE NATURE AND FATE OF PETROLEUM IN THE MARINE ENVIRONMENT. THE DISCUSSIONS ARE DIRECTED TOWARD RESEARCH WORKERS, ENVIRONMENTALISTS, ETC. CONCERNED WITH THE MANY ASPECTS OF PETROLEUM POLLUTION OF MARINE WATERS. ARCTIC, SUBARCTIC, HYDROCARBONS
REFV ARCTIC, SUBARCTIC, HYDROCARBONS
CODE T162 B
- AUTH HALINS D.C. (EDITED BY)
TITL EFFECTS OF PETROLEUM ON ARCTIC AND SUBARCTIC MARINE ENVIRONMENT AND ORGANISMS PART III: BIOLOGICAL EFFECTS
PUBL ACADEMIC PRESS
ABST IN THIS VOLUME AN ATTEMPT IS MADE TO COMPILE DATA, EVALUATE THE IMPLICATIONS TO POSSIBLE ALTERATIONS IN ORGANISMS AND ECOSYSTEMS AND OFFER SUGGESTIONS FOR FUTURE WORK WHERE SIGNIFICANT GAPS IN KNOWLEDGE EXIST.
REFV ARCTIC, SUBARCTIC, HYDROCARBONS
CODE T163 B
- AUTH HANN M.K., CLARK R.B.
TITL LONG TERM EFFECTS OF OIL SPILLS ON MARINE INTERTIDAL COMMUNITIES
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ABST THIS PAPER DISCUSSES THE RESULTS OF STUDIES OF LONG TERM EFFECTS OF OIL SPILLS ON THE MARINE INTERTIDAL COMMUNITIES.
REFV HYDROCARBONS, FOOD WEBS, LONG-LIVED CONTAMINANTS, RECOVERY
CODE Z669F
- AUTH HANSEN J.O.
TITL HEAVY DUTY OIL CONTAINMENT SYSTEM PNEUMATIC BARRIER SYSTEM
PUBL USCG, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. T14102/74/004
CODE 0751R
- AUTH MARASCHING R.J., TREYBAL R.E.
TITL THE COALESCENCE OF DROPS IN LIQUID-LIQUID FLUIDIZED BEDS
PUBL AIChE JOURNAL VOL. 17, NO. 5, SEPT 1971
ABST THE COALESCENCE RATES OF EQUISIZED DROPS OF ORGANIC LIQUIDS FLUIDIZED BY WATER UNDER CONDITIONS OF MUTUAL SATURATION WERE STUDIED. COALESCENCE, FLUIDIZATION, SATURATION
REFV CODE 0076F
- AUTH MARCH F.
TITL DYNAMIC REEL OIL CONTAINMENT
PUBL PHYSICAL REMOVAL
ABST RESULTS OF ANALYTICAL STUDIES AND MODELING TESTING ARE PRESENTED IN THIS PAPER.
REFV DYNAMIC REEL, BARRIERS, CONTAINMENT
CODE 0805F
- AUTH MARCH F.A.
TITL A PHYSICAL BARRIER TO CONTAIN SPILLED HAZARDOUS MATERIALS IN WATER COURSES
PUBL OCEAN SYSTEMS INC., FOR USEPA, NO. 68-01-0103, SSIE NO. 688-951-1
CODE 0494P
- AUTH MARCH F.A., BEACH R.
TITL TESTING OF A HIGH SEAS OIL RECOVERY SYSTEM
PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1750, APR. 29 - MAY 2, 1973
ABST A SYSTEM FOR RECOVERY OF PETROLEUM PRODUCTS FROM ACCIDENTAL OFFSHORE SPILLS HAS BEEN DEVELOPED AND TESTED.
REFV RECOVERY, HIGH EFFICIENCIES, RECOVERY RATE
CODE 0122F
- AUTH MARCH F.A., BEACH R.L.
TITL HIGH SEAS OIL RECOVERY SYSTEM
PUBL CONTROL TECHNOLOGY RESEARCH AND DEVELOPMENT
ABST A REPORT ON THE SYSTEM OF RECOVERY OF PETROLEUM PRODUCTS FROM ACCIDENTAL OFFSHORE SPILLS HAS BEEN DEVELOPED AND TESTED.
REFV CLEANUP, RECOVERY, CONTAINMENT
CODE 0545F
- AUTH MARINSKY D.
TITL DIFFERENTIAL VISCOSITY OIL FILTER
PUBL INT. REPT. OF MECHANICAL ENGINEERING
ABST A STUDY TO OBTAIN DATA ON THE SEPARATION OF AN OIL AND WATER EMULSION BY MEANS OF FILTRATION ALSO INCLUDED IS REPORT AND ARTICLE TITLED "DETERMINATION OF VOLATILE AND NONVOLATILE OILY MATERIAL. INFRARED SPECTROMETRIC METHOD."
REFV DIFFERENTIAL VISCOSITY OIL FILTER, SEPARATION, FILTRATION
CODE 0663R
- AUTH MARK H., MATSON J., GOLPACK R., TU T.C.
TITL IMPROVED ESTIMATION OF OIL CONTENT IN SEDIMENTS IN PRESENCE OF BIOLOGICAL MATTER
PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY, VOL. 6, SEPT. 1972
ABST THE CRUDE OIL CONTENT OF MARINE SEDIMENTS WAS DETERMINED BY IR SPECTROSCOPY FROM THE MAGNITUDE OF 2975 CM⁻¹ ABSORBANCE. CALCULATIONS MADE OF OIL CONTENT IN THE PRESENCE OF BIOLOGICAL MATERIALS. OIL CONTENT, DETERMINATION, INTERNAL REFLECTANCE SPECTROSCOPY
REFV CODE Z630F
- AUTH MARKEE A., BIANCHI R.A.
TITL PERFORMANCE TESTING OF PROTOTYPE SYSTEMS AND DEVICES DEVELOPED TO REMOVE AND SEPARATE SPILLED OIL
PUBL BETHLEHEM INTERNATIONAL, PRO API, SSIE NO. PAP-73 0466A
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- AUTH MARKS W., GESS C., MISHMAN J.
TITL THEORETICAL AND EXPERIMENTAL EVALUATION OF OIL SPILL CONTROL DEVICES
PUBL PHYSICAL REMOVAL
ABST THIS PAPER DESCRIBES THE FIRST PHASE OF A PROGRAM AIMED AT PROVIDING A MEANS FOR EVALUATION OF EXISTING OIL CONTAINMENT DEVICES AND FOR IMPROVING BASIC DESIGN.
REFV CONTAINMENT, BOOMS, BARRIERS
CODE 0812F
- AUTH MARTIN E.J., GUNTZ G.O.
TITL STATE OF MD. WASTE OIL RECOVERY AND REUSE PROG.
PUBL EPA 470/7-74-013, 6 PB 270001
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- AUTH MARR W.
TITL OIL SPILL
PUBL SIERRA CLUB, SAN FRANCISCO, 1971
ABST AN ECOLOGICAL VIEWPOINT OF THE HAZARDS OF COASTAL REFINERIES, SPILL, OIL, AND THE VULNERABILITY OF SUPERFUND SITES.
CODE 0022X
- AUTH MATSON J.S.
TITL EXCHANGE OF COMMENTS: SYSTEMS CHEMICAL ANALYSIS OF PETROLEUM POLLUTANTS
PUBL ANALYTICAL CHEMISTRY, VOL. 48, NO. 12, NOV. 1976
ABST THIS PAPER DISCUSSES OIL IDENTIFICATION, IDENTIFICATION, SYSTEMS CHEMICAL ANALYSIS, PRECISION
CODE 1230F
- AUTH MATSON J.S., GOLPACK R., MARK H., SCHUTT C.
TITL A RAPID NON-DESTRUCTIVE TECHNIQUE FOR INFRARED IDENTIFICATION OF CRUDE OILS BY INTERNAL REFLECTION SPECTROMETRY
PUBL AMERICAN CHEMICAL SOCIETY
ABST A REPORT OF AN INVESTIGATION INTO THE EFFECTS OF AN OIL BLOW OUT ON THE COAST OF THE SANTA BARBARA CHANNEL.
REFV INTERNAL REFLECTION SPECTROSCOPIC TECHNIQUE, IDENTIFICATION, DIFFERENTIATION
CODE Z630F
- AUTH MAUMER A., EDGERTON A.T.
TITL FLIGHT EVALUATION OF US COAST GUARD AIRBORNE OIL SURVEILLANCE SYSTEM
PUBL RTS JOURNAL VOL. 10, NO. 4, MAY 1974
ABST A PROTOTYPE AIRBORNE OIL SURVEILLANCE SYSTEM WAS DEVELOPED FOR THE US COAST GUARD BY AERDJET ELECTROSYSTEMS CO. THE MULTISENSOR SYSTEM PERMITS REAL-TIME, DAY-NIGHT, ALL-WEATHER DETECTION, MAPPING, AND DOCUMENTATION OF OIL SPILLS BY SEA. SURVEILLANCE, MULTISENSOR SYSTEM, DETECTION
REFV CODE 0124F
- AUTH MAUMER D.
TITL ENVIRONMENTAL VULNERABILITY OF THE DELAWARE BAY AREA TO DEEPWATER PORTS
PUBL UNKNOWN
ABST THE PURPOSE OF THIS PAPER IS TO BRIEFLY OUTLINE PROBABLE ENVIRONMENTAL EFFECTS AND PROBLEMS INVOLVED IN BUILDING AND COMPARING ENVIRONMENTAL VULNERABILITY.
REFV DEEPWATER PORTS, ENVIRONMENTAL VULNERABILITY, HYPOTHETICAL SCENARIO
CODE T201F
- AUTH MAUMER D.
TITL OFFSHORE TERMINAL OPERATION IMPACT
PUBL UNIV. OF DELAWARE, SCHOOL OF MARINE SCIENCE, SSIF NO. 689-1113
CODE 0470R
- AUTH MAVER E.
TITL THEORY OF LIQUID ATOMIZATION IN HIGH VELOCITY GAS STREAMS
PUBL IAS JOURNAL, DEC. 1961
ABST LIQUID ATOMIZATION BY HIGH VELOCITY GAS STREAMS IS INVESTIGATED ANALYTICALLY BY CONSIDERATION OF GAS-LIQUIDS INTERFACE BEHAVIOR IN THE REGIME OF CAPILLARY WAVE (TRIPPLE) PROPAGATION.
REFV LIQUID ATOMIZATION, HIGH VELOCITY GAS STREAMS, CAPILLARY WAVE
CODE 2574F
- AUTH MAVER J.P.

TITLE PLANNING FOR MINIMUM OIL SPILL RISK: ESTERO BAY
 PUBL STANDARD OIL CO OF CAL. FOR EPA 1975 CONFERENCE
 EFTY BISA, ESTERO BAY, PIPELINE
 CODE 0100

AUTH RAYO DONALD, PAGE D.S., CODIFY J., SORPSON E.,
 BRADLEY F., GILJILAN E.S., MARSO S.A.
 TITLE WEATHERING CHARACTERISTICS OF PETROLEUM
 HYDROCARBONS DEPOSITED IN FINE CLAY MARINE
 SEDIMENTS, SEASPOUT, NAINE
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST THIS PAPER REPORTS THE ANALYSIS OF COLLECTED
 SEDIMENT SAMPLES IN WHICH IT WAS POSSIBLE TO MAKE
 A COMPARISON WITH HYDROCARBON DATA COLLECTED IN
 THE PARLIER INVESTIGATION. IN ADDITION, AN
 ASSESSMENT OF THE CURRENT STATE OF RECOVERY OF
 LONG-LOVE FROM 1971 OIL SPILL IS CONSIDERED.
 EFTY GAS CHROMATOGRAPHY, WEATHERING, CLAY SEDIMENTS
 CODE 2669F

AUTH MATTHEWS E.E., BRUOP R.H.
 TITLE AVIATION FUEL SPILL CONTAINMENT USING ADSORBENT
 MATERIALS
 PUBL OML-TP-9, AD 776767
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AUTH MCNEIFF J.J., BRUM C.A.
 TITLE OCEAN BOTTOM ENVIRONMENTAL PARAMETERS FOR DEEP
 OCEAN SYSTEMS DESIGN, VOL. 111 - LITERATURE SURVEY
 INDEX
 PUBL OML, DEPT. OF OCEAN ENGINEERING, TECH. REPORT NO.
 4026-3, APRIL 1970
 ABST THE LITERATURE SURVEY PRESENTED IN THIS VOLUME
 WAS CONDUCTED AS PART OF AN INVESTIGATION TO
 DEFINE RECOMMENDATIONS FOR DEEP-OCEAN
 OCEANOGRAPHIC RESEARCH.
 EFTY DEEP OCEAN SYSTEMS, STATE OF THE ART KNOWLEDGE,
 CODE 6187F

AUTH MCALIFFE C.
 TITLE DETERMINATION OF C 1 - C 10 HYDROCARBONS IN WATER
 BY MEANS OF POLLUTION MONITORING, PROCEEDINGS OF A
 SYMPOSIUM AND WORKSHOP, MAY 13-17, 1976
 ABST THE METHOD REPORTED HERE IS BASED ON THE
 SUCCESSIVE GAS CHROMATOGRAPHIC ANALYSIS AFTER
 REPEATED EQUILIBRATION OF A HYDROCARBON-FREE GAS
 WITH AN AQUEOUS SAMPLE CONTAINING DISSOLVED
 HYDROCARBONS. ALL CLASSES OF HYDROCARBONS HAVING
 UP TO 11 CARBON ATOMS IN THE MOLECULE CAN BE
 DETERMINED.
 EFTY GAS CHROMATOGRAPHY, AQUEOUS SAMPLE, BIODEGRADATION
 CODE 2677F

AUTH MCALIFFE C.
 TITLE DETERMINATION OF DISSOLVED HYDROCARBONS IN
 SURFACE WATERS
 PUBL CHEMICAL GEOLGY, VOL. 4, 1969
 ABST THE CONCENTRATIONS AND DISTRIBUTIONS OF
 HYDROCARBONS DISSOLVED IN SURFACE BRINE HAS BEEN
 STUDIED WITH THE OBJECTIVE OF DETERMINING IF THE
 HYDROCARBONS CONTENT OF THE SAMPLED BRINE CAN BE
 USED TO DETERMINE IF AN EXPLORATORY WELL IS CLOSE
 TO OIL ACCUMULATION AND TO PROVIDE INFO TO HELP
 ANSWER QUESTIONS CONCERNING ORIGIN, MIGRATION AND
 ACCUMULATION OF PETROLEUM.
 EFTY PETROLEUM ACCUMULATION, ORIGIN OF PETROLEUM,
 CODE 2610F

AUTH MCALIFFE C.
 TITLE EVAPORATION AND SOLUTION OF C 7 TO C 10
 HYDROCARBONS FROM CRUDE OIL ON THE SEA SURFACE
 CHEMICAL FIELD RESEARCH CO.
 PUBL EXPERIMENTAL DATA ARE PRESENTED ON THE EVAPORATION
 AND SOLUTION OF LOW MOLECULAR-WEIGHT HYDROCARBONS
 FROM FOUR OIL SPILLS OF TWO DIFFERENT CRUDE
 OILS.
 EFTY TOXICITY, CONCENTRATION AND DEPOSITION, EVAPORATION
 CODE 2634F

AUTH MCALIFFE C.
 TITLE GC DETERMINATION OF SOLUTES BY MULTIPLE PHASE
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 PUBL CHEMICAL TECHNOLOGY, VOL. 1, JAN. 1971
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 EFTY MULTIPLE PHASE EQUILIBRIUM, DISTRIBUTION
 COEFFICIENTS, VAPOR PRESSURE
 CODE 2629F

AUTH MCALIFFE C.
 TITLE OIL-IN-WATER EMULSIONS AND THEIR FLOW PROPERTIES
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 TO IMPROVE OIL RECOVERY IN WATERFOODS.
 EFTY OIL IN WATER EMULSIONS, SELECTIVE PLUGGING AGENT,
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AUTH MCALIFFE C.

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AUTH MCALIFFE C.
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 EFTY EQUILIBRATING WATER, GAS PHASE, GAS CHROMATOGRAPHY
 CODE 2681F

AUTH MCALIFFE C.
 TITLE SOLUBILITY IN WATER OF PARAFFIN CYCLOPARAFFIN AND
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 CODE 2081F

AUTH MCALIFFE C.
 TITLE SOLUBILITY IN WATER OF PARAFFIN, CYCLOPARAFFIN,
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AUTH MCALIFFE C.
 TITLE SOLUBILITY IN WATER OF PARAFFIN, CYCLOPARAFFIN,
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 65 HYDROCARBONS HAVE BEEN MEASURED USING A
 GAS-LIQUID PARTITION CHROMATOGRAPHIC TECHNIQUE.
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 LOCATION OF THE SOLUBILITY IN WATER IS A LINEAR
 FUNCTION OF THE HYDROCARBON MOLECULAR VOLUME.
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 EFTY HYDROCARBONS, VAPOR PRESSURE, SOLUBILITY
 CODE 2633F

AUTH MCALIFFE C., PALMER L.L.
 TITLE ENVIRONMENTAL ASPECTS OF OFFSHORE DISPOSAL OF
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 PUBL SOCIETY OF PETROLEUM ENGINEERS OF AIME, SPE 5966-
 APR. 2-4, 1976
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 ENVIRONMENTALLY ACCEPTABLE METHOD FOR DISPOSAL OF
 DRILLING WASTES.
 EFTY DRILLING FLUID DISPOSURE, ENVIRONMENTAL EFFECTS,
 DISPOSAL OF DRILLING WASTE
 CODE 2621F

AUTH MCALIFFE C.D.
 TITLE DISPERSAL AND ALTERATION OF OIL DISCHARGED ON A
 WATER SURFACE
 PUBL CHEMICAL FIELD RESEARCH CO.
 ABST THE MOVEMENT AND ALTERATION OF OIL DISCHARGED ONTO
 A WATER SURFACE ARE DISCUSSED IN RELATION TO
 ENVIRONMENTAL EFFECTS, INCLUDING ARCTIC AND
 SUBARCTIC CONDITIONS. TECHNIQUES TO MINIMIZE
 POSSIBLE ADVERSE EFFECTS FROM OIL SPILLS ARE
 PROPOSED ALONG WITH SUGGESTED RESEARCH NEEDS.
 EFTY SPREADING AND MOVEMENT, EVAPORATION,
 CODE 2622F

AUTH MCALIFFE C.D.
 TITLE ENVIRONMENTAL ASPECTS OF OCS PETROLEUM DEVELOPMENT
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 FLUIDS AND CUTTINGS, AND OF THE PRODUCED WATER
 FROM COASTAL AND OFFSHORE OIL AND GAS EXPLORATION
 AND PRODUCTION WELLS ARE DISCUSSED. THESE
 DISCHARGES ARE REVIEWED AND PLACED IN PERSPECTIVE
 WITH OTHER DISCHARGE SOURCES. COSTS FOR ALTERNATE
 DISPOSAL OF DRILLING AND PRODUCTION DISCHARGES ARE
 CONSIDERED AND FOUND TO BE VERY EXPENSIVE AND
 ENVIRONMENTALLY UNNECESSARY.
 EFTY ENVIRONMENTAL ASPECTS, DISCHARGES, EXPLORATION
 CODE 2624F

AUTH MCALIFFE C.D.
 TITLE SURVEILLANCE OF THE MARINE ENVIRONMENT FOR
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 PUBL MARINE SCIENCE COMMUNICATIONS VOL. 2, NO. 1, 1976
 ABST THIS PAPER REVIEWS AND EVALUATES THE RESURVE
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 MARINE WATERS AND SEDIMENTS, AND COMPARES THESE
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 INPUTS. THE MECHANISMS THAT DESTROY HYDROCARBONS
 ARE DISCUSSED. AN ESTIMATE OF HYDROCARBON
 DISTRIBUTION IS GIVEN FOR THE NORTH ATLANTIC
 OCEAN.
 EFTY SURVEILLANCE, CONCENTRATIONS, WATER AND SEDIMENTS
 CODE 2625F

- AUTH MCKINNEY C.O., SHALLEY A.E., GARDNER B.O., JONES E.J.
 TITLE CHEVON MAIN PASS BLOCK OIL SPILL: CHEMICAL AND BIOLOGICAL INVESTIGATION
 PUBL PROCEEDINGS OF THE JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS SAN FRANCISCO, 1975
 ABST DURING A THREE WEEK PERIOD IN 1970 AN ESTIMATED 65,000 BARRELS OF 340 API GRAVITY CRUDE OIL WERE DISCHARGED FROM THE CHEVON MAIN PASS BLOCK AT C PLATON, 11 MILES EAST OF THE MISSISSIPPI RIVER DELTA. TWO THOUSAND BARRELS OF CHEMICAL DISPERSANTS WERE SPRAYED ON THE PLATFORM AND SURROUNDING WATER SURFACE.
 KEYW CHEMICAL AND BIOLOGICAL STUDIES, DISPERSANTS, DISCHARGE
 CODE 2676F
- AUTH MCKINNEY A.B., WIDDINS W.D., EPHRAIM W.D., HARRIS J.W., BROOK D.W., HERRS M.S., WANDERFULA J.P.
 TITLE BIOAVAILABILITY OF CRUDE OIL FROM EXPERIMENTALLY OILED SEDIMENTS TO ENGLISH SOLE (PARCOPMYS VENTRISI) AND PATHOLOGICAL CONSEQUENCES
 PUBL JOURNAL OF THE FISHERIES, VOL. 95, NO. 5, MAY 1978
 ABST ENGLISH SOLE WERE EXPOSED TO EXPERIMENTALLY OILED SEDIMENT FOR A 4 MONTH PERIOD TO ASSESS THE BIOAVAILABILITY AND TISSUE HYDROCARBON DISTRIBUTION KINETICS IN PLATISMA PLATYSSUM, PISCICULTURE, PATHOLOGY, ATMOSPHERIC HYDROCARBONS, BOTTOM SEDIMENTS, DIURNATION
 CODE 7669F
- AUTH MCKINTY J.A., WELDER E.J., DONLON J.S.
 TITLE STANDARD DISPERSANT EFFECTIVENESS AND TOXICITY TESTS
 PUBL ENVIRONMENTAL PROTECTION TECHNOLOGY SERIES, EPA-67-73-201, MAY 1973
 ABST A BRIEF HISTORY OF THE DEVELOPMENT OF THE STANDARD EPA DISPERSANT EFFECTIVENESS AND TOXICITY TEST IS OUTLINED. THE STANDARD TESTS ARE PRESENTED AND DISCUSSED. AN ANALYSIS OF VARIANCE IS PERFORMED ON THE DATA DEVELOPED BY THREE INDEPENDENT LABORATORIES IN ORDER TO DETERMINE THE REPRODUCIBILITY OF TEST PROCEDURES.
 KEYW DISPERSANTS, TOXICITY, TESTING
 CODE 7599F
- AUTH MCKINTY L.T., LINDLOF C.P., WALTER M.F.
 TITLE CHEMICAL DISPERSANT FOR THE CONTROL OF OIL SPILLS
 PUBL OIL SPILL 85
 ABST SYMPOSIUM WAS HELD AT WILLIAMSBURG, VA., OCT.-NOV. 1977. PAPERS PRESENTED ADDRESS TECHNOLOGICAL MATURITY, LABORATORY EFFECTIVENESS TOXICITY TESTING CONSIDERATIONS AND GENERAL NATURE OF DISPERSANTS
 KEYW DISPERSANTS, CRUDE OIL, TOXICITY TESTING, SAUTER MEAN DROP DIAMETER, MIXING ENERGY
 CODE 7723F
- AUTH MCKINCH A.L., GUNTER W., KNIGHT B.
 TITLE OIL ON WATER SENSOR
 PUBL TEXAS INSTRUMENTS FER, 1974
 ABST THE OIL ON WATER SENSOR SYSTEM DETECTS THE PRESENCE OF OIL ON WATER BY EMITTING A WIDENAND IN PULSE AND RECEIVING REFLECTIONS AT 2 NARROW SPICAL BANDS.
 CODE 6126F
- AUTH MCKON D.L., HARRISON W., FINNEN B.
 TITLE WATER RESOURCES RESEARCH PROGRAM, TRANSPORT AND DISPERSION OF OIL SPILLAGE WASTES IN THE COASTAL WATERS OF SOUTHWESTERN LAKE MICHIGAN
 PUBL ENERGY AND ENVIRONMENTAL SYSTEMS DIVISION, AM/CP 76-4, W-31-120-ENG-10, JULY 1976
 ABST THIS REPORT IS THE FIRST OF A SERIES THAT WILL BE DEVOTED TO THE TRANSPORT AND DISPERSION OF OILY WASTES DISCHARGED INTO THE COASTAL WATERS OF S.W. LAKE MICHIGAN.
 KEYW DISCHARGE, SURFACE PLUM, DISPERSION, TRANSPORT
 CODE 6352F
- AUTH MCKON D.L., SANDERS A.D., ALPHEUS J.W., OTHMAN J.C., HARRISON W.
 TITLE TRANSPORT OF OILY POLLUTANTS IN THE COASTAL WATERS OF LAKE MICHIGAN: AN APPLICATION OF RAPE EARTH TRACERS
 PUBL MICHIGAN NATIONAL LABORATORY, ENERGY AND ENVIRONMENTAL SYSTEMS DIVISION
 ABST A METHOD WAS DEVELOPED FOR TRACING OILY WASTE WITH BYSSOBIUM AND THE ASSOCIATED PRESH WATER WITH BARIUM. THE METHOD WAS APPLIED IN TWO FIELD EXPERIMENTS THAT INVOLVED TRACING OILY WASTES AND POLLUTED WATER FROM THE INDIANA HARBOR CANAL RACE INTO LAKE MICHIGAN.
 KEYW RAPE EARTH ELEMENTS NEUTRUM ACTIVATION ANALYSIS BYSSOBIUM, BARIUM, OILY WASTE, OIL TRACING, WATER TRACING
 CODE 7717 F
- AUTH MCKRACKEN B.E.
 TITLE HYDRODYNAMICS OF DIVERSIONARY BOOMS
 PUBL MASH AND MANGER-SILDS MASH CO., INC.
 ABST THE FAILURE OF BOOMS TO CONTAIN FLOATING OIL ON CURRENTS ABOVE 0.5 M/S APPEARS TO BE WELL ESTABLISHED. A METHOD SUGGESTED TO SURMOUNT THIS LIMITATION OF CURRENTS UNDER CONTAINMENT AND REMOVAL CAN BE ACCOMPLISHED. THIS REPORT
- DESCRIBES FULL SCALE TESTING OF THE FLOW FIELD (BOOM) A COMMERCIAL OIL BOOM. THE METHODS, RESULTS, AND TECHNIQUES DESCRIBED ARE OF INTEREST TO THOSE INTERESTED IN SPECIFYING, USING OR TESTING SUCH EQUIPMENT.
 KEYW FLOW FIELD, OIL SPILL BOOM, ENTRAINMENT
 CODE 7728F
- AUTH MCKENNTI J.
 TITLE IDENTIFYING NATURAL GAS TECHNOLOGY
 PUBL CHEMICAL TECHNOLOGY REVIEW NO. 10, NOV'S DATA COMP. PARA 81021, NJ, 1973
 ABST THIS PAPER SUPPLIES DETAILED CHEMICAL INFORMATION AND CAN BE USED AS A GUIDE TO THE US PATENT LITERATURE IN THIS FIELD.
 KEYW LNG TECHNOLOGY, CHEMICAL INFORMATION, PATENT INFORMATION
 CODE 4015E
- AUTH MCKEPPER L.F.
 TITLE WAVE MEASUREMENT SYSTEMS
 PUBL THE JOHN MCPHAIN GRAVITYHYDRODYNAMICS LAB. REPORT NO. 1 SEPT. 1964
 ABST THIS REPORT DESCRIBES TWO DIFFERENT LINEAR TYPES OF SYSTEMS FOR MEASURING SURFACE WAVES. ONE IS BEST SUITED FOR LAB WORK, THE OTHER, FIELD WORK.
 CODE 6047F
- AUTH MCKEY W.C.
 TITLE EVALUATION OF SURFACTANTS, SORBENTS AND SINKING AGENTS AS EFFECTIVE OIL SPILL CLEANUP AGENTS
 PUBL GOVERNMENT REPORTS ANNOUNCEMENTS 73101121
 CODE 1076F
- AUTH MCKEY W.C.
 TITLE EVALUATION OF SURFACTANTS, SORBENTS, AND SINKING AGENTS AS EFFECTIVE OIL SPILL CLEANUP AGENTS
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 CODE 0679F
- AUTH MCKEY W.C., DIXON G.L., JORDON B.L.
 TITLE EFFECTS OF TILMATION OF OIL SLICES
 PUBL OFFICIAL GAZETTE OF US PATENT OFFICE, VOL. 927, NO. 4, OCT. 22, 1974
 ABST REMOVAL OF OILS BY FREEZE-DRYING BY MICROORGANISMS ALONG WITH NUTRIENTS, ZIMICOCORGANISMS WITHIN A CARRIER MATRIX BY MICROORGANISMS WITHIN A CARRIER ALONG WITH NUTRIENTS.
 CODE 3127F
- AUTH MCKEY W.C.
 TITLE THE BEHAVIOR OF OIL SPILLED IN A COLD WATER ENVIRONMENT
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1527, MAY 1-3, 1977
 ABST THIS PAPER DEALS WITH THE WAY IN WHICH OIL BEHAVES WHEN IT INTERACTS WITH THE COLD ENVIRONMENT AND THE EFFECT OF TANK INTERFERENCE ON THE EFFECTIVENESS OF CLEANUP TECHNIQUES.
 KEYW CLEANUP, ENVIRONMENTAL IMPACT, RECOVERY
 CODE 0570F
- AUTH MCKEY W.C., BETHANOUR D.J.
 TITLE PHYSICAL AND CHEMICAL CHANGES IN SPILLED OIL WEATHERING UNDER NATURAL CONDITIONS
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 ABST THIS PAPER DISCUSSES THE STUDY OF LONG TERM BEHAVIOR OF SPILLED OIL WEATHERING UNDER NATURAL CONDITIONS.
 KEYW ENVIRONMENTAL IMPACT, DIFFUSION, EVAPORATION, BIODEGRADATION
 CODE 0653F
- AUTH MCKEY W.C., MCKEY D.A.
 TITLE THE PROPERTIES OF SARLE ISLAND CRUDE OIL IN RELATION TO ITS BEHAVIOR IN THE EVENT OF A SPILL
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1091, MAY 6-8, 1974
 ABST DISCUSSION OF RELATIONSHIP OF PROPERTIES OF OIL TO THE FOLLOWING PROCESSES: OXIDATION, EVAPORATION, FRACTIONATION, DISPERSION, SOLUTION
 KEYW OXIDATION, EVAPORATION, FRACTIONATION, DISPERSION, SOLUTION
 CODE 0658F
- AUTH MCKEY W.C., MCKEY D.A.
 TITLE RESULTS OF GREAT PASSMORE ARCTIC OIL SPILLS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1527, MAY 1-3, 1977
 ABST THIS PAPER DISCUSSES THE EFFECTIVENESS OF AVAILABLE CHEMICAL, MECHANICAL, AND DESTRUCTIVE CLEANUP TECHNIQUES FOR OIL RECOVERY UNDER ARCTIC CONDITIONS.
 KEYW RECOVERY, CLEANUP, CONTINGENCY
 CODE 0582F
- AUTH MCKEY W.C., CONNELL D.W.
 TITLE TOXICITY OF THE OIL DISPERSANT CORBIT 7004 TO CERTAIN AUSTRALIAN MARINE ANIMALS.
 PUBL SEARCH, 8:227-224
 CODE 1012F
- AUTH MCKEY T.J.
 TITLE OIL SPILL BEHAVIOR IN A WINTER ARCTIC ENVIRONMENT

- PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1747, APRIL 2-4, 1971
 ABST THIS PAPER DISCUSSES THE RESEARCH PROGRAM INITIATED TO DETERMINE THE RATE AND BEHAVIOR OF CRUDE OIL DISCHARGES IN AN ARCTIC ENVIRONMENT.
 KEYW OIL SPREADING AND AGING ON ICE, INTERACTION OF SURF AND OIL, EFFECTIVENESS OF RECOVERY TECHNIQUES
 CODE 0578
- AUTH KENNETH T.J., GOLDEN P.
 TITL BEHAVIORAL CHARACTERISTICS AND CLEANUP TECHNIQUES OF NORTH SLOPE CRUDE OIL IN THE ARCTIC WINTER ENVIRONMENT
 PUBL USCG, 1973 JOINT CONFERENCE
 KEYW BEHAVIORAL CHARACTERISTICS, CLEANUP, NORTH SLOPE CRUDE OIL, ARCTIC ENVIRONMENT
 CODE 02957
- AUTH MCKEY B.M.
 TITL OIL SLICK DISPERSION APPARATUS
 PUBL US PATENT OFFICE
 CODE 50204
- AUTH MERRILL C.S.L., PEG P.
 TITL ON-LINE COMPUTER SYSTEMS FOR ENVIRONMENTAL EMERGENCY MANAGEMENT
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- AUTH NICHOLAS B.J., MEYERS T.J., BOLPACK R.L.
 TITL MICROBIAL DECOMPOSITION PATTERNS USING CRUDE OIL THE MICROBIAL DEGRADATION OF OIL POLLUTANTS CENTER FOR PETROLEUM RESEARCH, 61515-79-01, 1973
 ABST A REPORT OF WEATHERED OILS COLLECTED FROM SOUTHERN CALIFORNIA BEACHS.
 KEYW CHROMATOGRAMS, WEATHERING OIL, MICROBIAL DECOMPOSITION
 CODE 26377
- AUTH WEI C.
 TITL RESONANT SCATTERING BY A NARROW WITH TWO COUPLED BASINS
 PUBL JOURNAL OF ENGINEERING MATH., VOL. 10, 1972
 ABST A NARROW WITH COUPLED RECTANGULAR BASINS IS SUBJECTED TO PERIODIC INCIDENT WAVES. IGNORING FRICTION THE SCATTERING PROBLEM IS SOLVED BY THE METHOD OF MATCHED ASYMPTOTICS FOR NARROW JUNCTIONS.
 KEYW RECTANGULAR BASINS, SCATTERING THEORY, WAVES
 CODE 76007
- AUTH REIJES P.M., JONGHLOOD L.J., TRIPRA, M.J.
 TITL NEW METHODS FOR COMBATING OIL SLICKS
 PUBL EXPLORATION AND PRODUCTION LAB ROYAL DUTCH SHELL, THE NETHERLANDS, 1969 JOINT CONFERENCE,
 COMBATING, METHODS
 CODE 02638
- AUTH RELLOR G.L., VANANDA I.
 TITL A HIERARCHY OF TURBULENCE CLOSURE MODELS FOR PLANETARY BOUNDARY LAYERS
 PUBL JOURNAL OF THE ATMOSPHERIC SCIENCES, VOL. 31, OCT. 1974
 ABST THIS PAPER DISCUSSES SIMPLIFICATION OF TURBULENCE MODELS.
 KEYW TURBULENCE, TURBULENCE MODELS, PLANETARY BOUNDARY LAYERS
 CODE 12147
- AUTH MELVIN P., BRUNSPECH H.
 TITL OIL SPILL AND OIL POLLUTION REPORTS MAY 1974 - JULY 1974
 PUBL USFPA INDUSTRIAL ENVIRONMENTAL RESEARCH LAB., OFFICE OF RESEARCH AND DEVELOPMENT, EPA 600/2-74-266, OCT. 1974
 ABST EIGHTEEN QUARTERLY COMPILATION OF SUMMARIES OF OIL SPILL EVENTS, CURRENT RESEARCH PROJECTS, LITERATURE CITATIONS, PATENTS.
 KEYW REPORTS, PUBLICATIONS, PATENTS, RESEARCH PROJECT CONFERENCES
 CODE 70058
- AUTH MENSING A.
 TITL USE OF VORTEX FLOW TO SEPARATE OIL FROM WATER MIXTURE
 PUBL DOT CG 00544, UNITED AIRCRAFT RESEARCH LAB., NOV. 1970
 CODE 08004
- AUTH MENSING A.E., STOEFFLER A.E., DAVIDSON S.A., REDDIEY T.E.
 TITL FINAL REPORT, INVESTIGATION OF THE USE OF A VORTEX FLOW TO SEPARATE OIL FROM AN OIL-WATER MIXTURE.
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 ABST STUDIES WERE MADE TO DETERMINE THE SIZE AND WEIGHTS OF COMPONENTS FOR FULL SIZE VORTEX SEPARATORS.
 KEYW CLEANUP, VORTEX FLOWS, VORTEX SEPARATORS, SKIMMERS
 CODE 08007
- AUTH MERTENS E.B.
 TITL RITE AND EFFECTS OF OIL IN THE ENVIRONMENT
 PUBL PRESENTED BEFORE THE U.S. DEPT. OF INTERIOR, BUREAU OF LAND MANAGEMENT MEETING, FEB. 6-8, 1975
 ABST STATEMENT BY THE AUTHOR IN REGARD TO THE PROPOSED
- INCREASE IN ACRFAY TO BE OFFERED FOR OIL AND GAS LEASING ON THE OUTER CONTINENTAL SHELF.
 KEYW ENVIRONMENTAL PROBLEMS, CONTAMINATION, LEASING
 CODE 70187
- AUTH MERTENS E.B., GUILD J.P.
 TITL THE EFFECTS OF OIL ON MARINE LIFE: AN OVERVIEW OF RESEARCH SPONSORED BY THE AMERICAN PETROLEUM INSTITUTE
 PUBL CHEVRON RESEARCH CO.
 ABST THIS PAPER IS CONCERNED ONLY WITH THOSE STUDIES RELATING TO THE PART OF THE OVERALL PROBLEM OF OIL SPILLS - THE EFFECTS OF OIL ON MARINE LIFE, MARINE LIFE, EFFECTS, STUDIES
 KEYW
 CODE 76777
- AUTH REYNOLDS P.J.
 TITL A HYDROBIOLOGICAL SURVEY OF A SMALL SPANISH RIVER/ STREAM POLLUTED BY OIL REFINERY AND PETROCHEMICAL WASTES
 PUBL FRESHWATER BIOLOGY, 26(1):50-57, 1973
 CODE 12577
- AUTH REYS P.M.
 TITL NEW METHODS FOR COMBATING OIL SLICKS
 PUBL 1969 JOINT CONFERENCE
 CODE 21148
- AUTH MICHAEL A.D.
 TITL THE EFFECTS OF PETROLEUM ON MARINE POPULATION AND COMMUNITIES
 PUBL UNPUBLISHED
 ABST THIS PAPER DISCUSSES THE EFFECTS OF OIL AS THEY CONCERN ORGANISMS IN THEIR NATURAL SURROUNDINGS, FIELD STUDIES OF COMMUNITIES AND POPULATIONS, LIVING ORGANISMS, RECOVERY, MARINE COMMUNITIES
 KEYW
 CODE 71327
- AUTH MICHAEL A.D., VAN BABEL C.R., BROWN L.S.
 TITL LONG-TERM EFFECTS OF AN OIL SPILL AT WEST PALM BEACH, FLA.
 PUBL MARINE BIOLOGICAL LAB., WOODS HOLE, MASS. FOR EPA 1974 CONFERENCE
 ABST PAPER INCLUDES: METHODS, HYDROCARBON ANALYSIS, AND BIOLOGICAL EFFECTS AND RESULTS.
 KEYW METHODS, LONG-TERM EFFECTS, BIOLOGICAL EFFECTS AND RESULTS
 CODE 015044
- AUTH MIGHT R.J., OPPENHEIMER E.M., KATZ J.E., LAROCK R.L.
 TITL MICROBIAL DEGRADATION OF NORMAL PARAFFIN HYDROCARBONS IN CRUDE OIL
 PUBL IN APPLIED CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS, API
 CODE 50200
- AUTH MIGHT R.J., ALLEN A.A., SCHLUTER R.S.
 TITL INVESTIGATION OF THE NATURE, EXTENT AND RATE OF NATURAL OIL SEEPAGE OFF SOUTHERN CALIFORNIA ONSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1549, MAY 1-3, 1972
 ABST THIS PAPER DISCUSSES THE OIL AND GAS SEEPS BEING INVESTIGATED BY USE OF AERIAL, SURFACE AND UNDERWATER SURVEY TECHNIQUES.
 KEYW OCEAN FLOOR CONDITIONS, MODES OF OIL RELEASE, SEEPAGE FLOW RATES
 CODE 08487
- AUTH MIGHT R.J.
 TITL ENVIRONMENTAL APPLICATIONS OF THE WEIBULL DISTRIBUTION FUNCTION: OIL POLLUTION SCIENCE, VOL. 176, JUNE 1972
 ABST THE WEIBULL DISTRIBUTION FUNCTION APPEARS TO BE A POWERFUL TOOL FOR THE STATISTICAL ANALYSIS AND INTERPRETATION OF ENVIRONMENTAL POLLUTION DATA. TO ILLUSTRATE ITS POTENTIAL, THE METHOD IS APPLIED TO A VARIETY OF OIL POLLUTION TOPICS, OTHER APPLICATIONS ARE SUGGESTED.
 KEYW SAMPLING, CONCENTRATION, ENVIRONMENTAL POLLUTION ANALYSIS, WEIBULL DISTRIBUTION FUNCTION
 CODE 21007
- AUTH RELES D.M., COUGH R.J., BROWN L.B.
 TITL THE ESTIMATION OF THE AMOUNT OF EMPIRE MIX CRUDE OIL IN MULLET, SWAMP, AND OYSTERS BY LIQUID CHROMATOGRAPHY
 PUBL DEPT. OF CHEMISTRY AND MICROBIOLOGY, MISS. STATE UNIV., FOR THE EPA 1975 CONFERENCE
 KEYW EMPIRE MIX CRUDE OIL, MULLET, SWAMP, OYSTERS, LIQUID CHROMATOGRAPHY
 CODE 08678
- AUTH BELGRAN H.J.
 TITL COMBINED EFFECTS OF WAVES AND CURRENT ON PERFORMANCE OF OIL BARRIERS, OIL POLLUTION RIT FOR USCG, BSIE NO. 62-12116
 CODE 04399
- AUTH BELGRAN J.
 TITL BEING PREPARED FOR FUTURE ARCO MERCHANTS NATIONAL OCEAN AND ATMOSPHERIC ADMINISTRATION, APR. 1977, RIT SEA GRANT PROGRAM, RITSC 77-10, SC 04-154-000-1
 ABST THIS REPORT GIVES POSSIBLE MEANS FOR DEALING WITH OIL EVENTS AND WITH STRIKE EVENTS BY CONSIDERING

PUBL U.S. COAST GUARD TECHNICAL REPORT
 ABST A METHOD TO MANUALLY CALCULATE THE LOCAL WIND
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 BASED ON TIME-DEPENDENT BERAN DYNAMICS. THE
 METHOD IS TUNED AND TESTED AGAINST A 2 1/2 MONTH
 LONG CURRENT AND WIND RECORD IN THE NORTH
 ATLANTIC.

KEYW WIND CURRENTS, BERAN, WIND DRIFT
 CODE 7727F

AUTH MOORE S., Dwyer P.
 TITLE EFFECTS OF OIL ON MARINE ORGANISMS: A CRITICAL
 ASSESSMENT OF PUBLISHED DATA
 PUBL WATER RESEARCH, VOL. 8, 1974
 ABST THIS PAPER DISCUSSES EFFECTS OF OIL ON MARINE
 ORGANISMS.

KEYW MARINE ENVIRONMENT IMPACT, TOXICITIES, BIOLOGICAL
 HABITATS
 CODE 1205I

AUTH MOORE S., Dwyer P., GATT A.
 TITLE A PRELIMINARY ASSESSMENT OF THE ENVIRONMENTAL
 VULNERABILITY OF MACHIAS BAY, MAINE, TO OIL
 SUPERTANKERS
 PUBL U.S.T., DEPT. OF CIVIL ENGINEERING, REPORT NO.
 167, JAN. 1973
 ABST THIS REPORT DISCUSSES THE PRELIMINARY ASSESSMENT
 OF THE ENVIRONMENTAL VULNERABILITY OF MACHIAS BAY,
 MAINE, TO OIL SUPERTANKERS.

KEYW SUPERTANKERS, INDIVIDUAL, POPULATION, COMMUNITY,
 ECOSYSTEMS
 CODE 0834F

AUTH MOORE S.F.
 TITLE SOME ASPECTS OF OFFSHORE TERMINAL SITE SELECTION
 IN NORTHERN NEW ENGLAND COASTAL AREAS

PUBL UNKNOWN
 ABST THE RESEARCH DESCRIBED HERE IS PART OF A STUDY IN
 WHICH THE PRIMARY OBJECTIVE IS TO ASSESS THE
 ENVIRONMENTAL VULNERABILITY OF THE MACHIAS BAY
 REGION, TO A HYPOTHETICAL SUPERTANKER TERMINAL.
 IMPORTS, TANKERS, DEWATER PORTS

KEYW
 CODE 7200F

AUTH MOORE S.
 TITLE DISPERSANTS OF OIL SLICKS IN PORTS AND AT SEA
 PUBL INTERNATIONAL CONFERENCE ON OIL POLLUTION OF THE
 SEA, OCT. 1964
 CODE 5010P

AUTH MORGAN R.L.
 TITLE A RAPID METHOD OF DETERMINING BUNKER C FUEL OIL IN
 MARINE ORGANISMS

PUBL BULLETIN OF ENVIRONMENTAL CONTAMINATION AND
 TOXICOLOGY VOL. 14, NO. 3,
 CODE 5047F

AUTH MURPHY R.J.
 TITLE THE ARGO MERCHANT OIL SPILL - A SCIENTIFIC
 ASSESSMENT - APRIL 1974
 PUBL SCIENCE APPLICATIONS, INC.
 ABST THIS REPORT PROVIDES A FINAL ANALYSIS AND
 EVALUATION OF THE SCIENTIFIC INVESTIGATIONS
 CONDUCTED BY VARIOUS FEDERAL, STATE AND PRIVATE
 AGENCIES FOLLOWING THE ARGO MERCHANT OIL SPILL IN
 DECEMBER 1971. IT DOCUMENTS PHYSICAL, CHEMICAL
 AND BIOLOGICAL INVESTIGATIONS, AS WELL AS RESEARCH
 INTO THE SCIENTIFIC EFFECTS OF THE SPILL.

KEYW ARGO MERCHANT, OIL SPILL
 CODE 7752F

AUTH MCGUIRE T.L.
 TITLE PREPARATION OF AN OIL SPILL PREVENTION TRAINING
 PROGRAM

PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL
 POLLUTION
 ABST THIS PAPER HIGHLIGHTS ITEMS NECESSARY TO DEVELOP A
 PACKAGE LEARNING PROGRAM ON SPILL PREVENTION,
 PREVENTION, IMPROVEMENT, KNOWLEDGE, TERMINAL
 OPERATORS

CODE 0814F

AUTH MOSTRY A.
 TITLE THE AGE OF THE OILING
 PUBL MAY ISSUE OF APRIL 1974
 ABST DISCUSSION OF OIL SPILLS IN HAZARDOUS CONDITIONS,
 TANKER TRANSPORT, SUPERTANKERS, OIL DUMPING

CODE 2700F

AUTH MURDER D.S., VARLEY A.
 TITLE A BIBLIOGRAPHY ON MARINE AND ESTUARINE OIL
 POLLUTION
 PUBL MARINE POLLUTION INFORMATION CENTRE, MARINE
 BIOLOGICAL ASSOCIATION OF THE U.S., JUNE 1975
 ABST THIS REPORT IS A SUPPLEMENT TO "A BIBLIOGRAPHY ON
 MARINE AND ESTUARINE OIL POLLUTION" OF SEPT. 1971.
 BIBLIOGRAPHY, MARINE, ESTUARINE

CODE 4071B

AUTH MURPHY P.
 TITLE A STUDY OF THE HYDROGRAPHY AND WIND-INDUCED
 CURRENTS IN EASTERN BRINE WILLIAM SOUND
 PUBL UNIV. OF ALASKA, SEASIDE, 1974
 CODE 0440B

AUTH MURPHY P.

KEYW WIND STRESS ON WATER; AN HYPOTHESIS
 PUBL SCRIPTS INSTITUTE OF OCEANOGRAPHY, UNIVERSITY OF
 CALIFORNIA, FEB. 1955.

ABST THIS PAPER DISCUSSES WIND STRESS ON WATER.
 KEYW FORM DRAG, WIND SPEED, TWO DIMENSION SPECTRUM
 CODE 6590F

AUTH MURPHY J.W.
 TITLE EFFECTS OF OFFSHORE OIL AND NATURAL GAS
 DEVELOPMENT ON THE COASTAL ZONE
 PUBL LIBRARY OF CONGRESS STUDY, AD HOC SELECT COMMITTEE
 ON OUTER CONTINENTAL SHELF, HOUSE OF
 REPRESENTATIVES, MARCH 1976
 ABST STUDY ON ONSHORE EFFECTS OF OFFSHORE OIL AND GAS
 DEVELOPMENT.

KEYW GAS AND OIL RESERVES, ENVIRONMENTAL AND
 SOCIOECONOMIC EFFECTS, REGULATIONS
 CODE 2511F

AUTH MURPHY T.A.
 TITLE ENVIRONMENTAL EFFECTS OF OIL POLLUTION
 PUBL JOURNAL OF THE SANITARY ENGINEERING DIV., ASCE
 PROCEEDINGS VOL. 97, NO. 543, PAPER 8771, JUNE
 1971
 CODE 5011P

AUTH MURPHY T.A., MCCARTHY L.T.
 TITLE EVALUATION OF THE EFFECTIVENESS OF OIL DISPERSING
 CHEMICALS

PUBL UNKNOWN
 ABST THIS PAPER DISCUSSES THE PROBLEMS OF THE
 EFFECTIVENESS OF OIL DISPERSING CHEMICALS WHICH
 HAS BEEN DEVELOPED.

KEYW DISPERSANTS, TOXICITY, ENVIRONMENTAL EFFECTS
 CODE 2115F

AUTH MURPHY S.P.
 TITLE OCEANOGRAPHIC OBSERVATION AND THEORETICAL ANALYSIS
 OF OIL SLICKS DURING THE CHEVRON SPILL

PUBL BCS
 ABST OCEANOGRAPHIC OBSERVATIONS NEAR THE CHEVRON
 SPILLINGS WEL OFF THE MISSISSIPPI DELTA IN MARCH
 1970

KEYW OBSERVATIONS, CHEVRON SPILL, SLICKS
 CODE 2570B

AUTH MURPHY S.P.
 TITLE TURBULENT DIFFUSION OF OIL IN THE OCEAN
 PUBL LIMNOL. OCEANOGRAPHY, VOL. 17, 1972
 CODE 2040P

AUTH MURPHY S.P.
 TITLE WIND AND CURRENT EFFECTS ON LARGE-SCALE OIL SLICKS
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2304,
 MAY 4-8, 1974

ABST THIS PAPER DISCUSSES THE EFFECTS OF WIND, WINDS
 AND SURFACE CURRENTS IN DETERMINING MOVEMENT OF
 OIL SLICKS.

KEYW WINDS AND CURRENTS, WIND SHIFTS, DENSITY FRONTS
 CODE 0857F

AUTH MURPHY T., BHANDARVAJ R.L.
 TITLE SIMULATION OF MOVEMENT OF OIL SLICKS IN THE STRAIT
 OF GEORGIA USING SIMPLE ATMOSPHERE AND OCEAN
 DYNAMICS

PUBL PART OF OIL
 ABST THIS PAPER DISCUSSES THE HYDRODYNAMICAL TECHNIQUES
 USED TO INVESTIGATE THE MOVEMENT OF OIL SLICKS.
 KEYW HYDRODYNAMICS, WIND AND WAVE CURRENT, OIL SLICK
 MOVEMENT
 CODE 0861F

AUTH MURPHY T.S.
 TITLE THE MOVEMENTS OF OIL SLICKS
 PUBL BAPP. P. - U. REUN. CONS. INT. EXPLOR. MAR. VOL.
 147, 1974
 CODE 2042P

AUTH MURPHY T.S., BARBER F.C.
 TITLE RIP CURRENT PATTERNS IN OIL SLICKS
 PUBL PROCEEDINGS OF THE FIRST CANADIAN SYM. ON REMOTE
 SENSING, VOL. 1 FEB. 1972
 CODE 2041P

AUTH MURPHY T.S., BHANDARVAJ R.L.
 TITLE APPLICATION OF THE CONCEPT OF RECTILINEAR MOTIONS
 TO THE MOVEMENT OF OIL SLICKS
 PUBL CANADA MARINE SCIENCES DIRECTORATE, MANUSCRIPT
 REPORT SERIES 32
 CODE 0315A

AUTH MACCELL B., MOTINI W.
 TITLE TOXICITY OF F.O.P. OIL DISPERSANTS TO SOME ANIMALS
 FROM THE BALTIC SEA
 PUBL MAR. BIOL., 20:237-243, 1974
 CODE 1022B

AUTH MASH A.E.R., MANN D.E., OLSEN P.C.
 TITLE OIL POLLUTION AND PUBLIC INTEREST: A STUDY OF THE
 SANTA BARBARA OIL SPILL
 PUBL INSTITUTE OF GOVERNMENTAL STUDIES, UNIV. OF CAL.
 1977

ABST THIS DISCUSSION OF THE SANTA BARBARA OIL SPILL HAS
 SOME PERTINANT INFORMATION ON PREVENTION AND
 REMEDIAL ACTION AND FEDERAL AND STATE LEGISLATION.
 CODE 0800P

- AUTH NAWMAC
 TITLE INTEGRATED LOGISTICS SUPPORT PLAN FOR HARBOR OIL SPILL RECOVERY SYSTEMS
 PUBL NAWMAC 115P-001
 ABST REFLECTS NAWMAC'S PHILOSOPHY OF A COMPLETE SYSTEMS APPROACH - FOR THE PLANNING, ANALYZING, DESIGNING, AND MANAGEMENT OF LOGISTICS RELATED DISCIPLINES IN SUPPORT OF THE ACQUISITION OF EQUIPMENT.
 CODE 91404
- AUTH NEAL R.W., JOHNSON E.E., BIANCHI P.A.
 TITLE THE DESIGN AND DEMONSTRATION OF A REMOTE-CONTROLLED HIGH SEAS OIL RECOVERY SYSTEM
 PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
 ABST THE OBJECT OF THE PROGRAM WAS TO DEMONSTRATE AND TEST A SPILLED OIL RECOVERY SYSTEM UNDER OFFSHORE CONDITIONS.
 KEYS REMOTE-CONTROL SKIMMER, RECOVERY, OFFSHORE CONDITIONS
 CODE 05577
- AUTH NERREY E., RODRIGUES S., MIKOLAJ P.
 TITLE PRELIMINARY RECOVERY OF FLOATING OIL
 PUBL UNPUBLISHED
 ABST A CONCEPT EMPLOYING A PUMP VORTEX FOR USE IN RECOVERING OIL FROM HIGH SEAS OIL SPILLS IS PRESENTED.
 KEYS PUMP VORTEX, RECOVERY, IMPELLERS
 CODE 91159
- AUTH NEFF J.W., ANDERSON J.
 TITLE AN ULTRAVIOLET SPECTROPHOTOMETRIC METHOD FOR THE DETERMINATION OF NAPHTHALENE AND ALKYLNAPHTHALENES IN THE TISSUES OF OIL CONTAMINATED MARINE ANIMALS
 PUBL BULLETIN OF ENVIRONMENTAL CONTAMINATION AND TOXICOLOGY, VOL. 14, NO. 1, 1975
 ABST THIS PAPER DESCRIBES A DIRECT SPECTROPHOTOMETRIC METHOD FOR THE SEMIQUANTITATIVE DETERMINATION IN SEA WATER AND THE TISSUES OF MARINE ANIMALS.
 KEYS TOXICITY, CHRONOTOXIC - 0555, SPECTROPHOTOMETRIC ANALYSIS
 CODE 25717
- AUTH NEFF J.W., ANDERSON J.W.
 TITLE ACCUMULATION, RELEASE AND DISTRIBUTION OF BENZO (A) PYRENE - C 14 IN THE CLAR BANGIA CUMENTA
 PUBL DEPT. OF BIOLOGY, TEXAS A & M UNIVERSITY FOR EPA 1975 CONFERENCE
 KEYS ACCUMULATION, RELEASE, DISTRIBUTION BENZ PYRENE, CLAR
 CODE 81349
- AUTH NELSON-SMITH A.
 TITLE EFFECTS OF OIL POLLUTION AND PURIFIED CLEANING ON SHORELIFE IN SOUTHWEST BRITAIN
 PUBL J. APPL. ECOL. 9:97-107
 CODE 10434
- AUTH NELSON-SMITH A.
 TITLE THE PROBLEM OF POLLUTION OF THE SEA
 PUBL O.C. MAR. BIOL. 8:2-15-304
 CODE 10904
- AUTH NEWMAN D.E., MACBETH M.L.
 TITLE OIL BOOMS AT A TIDAL INFLET
 PUBL HYDRAULIC RESEARCH STATION, REPORT NO INT 118, 1971
 CODE 87368
- AUTH NICHOL C.W.
 TITLE THE NIZHNSHINA OIL SPILL - A TRAGEDY FOR JAPAN AND A LESSON FOR CANADA
 PUBL DEPT. OF THE ENVIRONMENT, OPS NO. EPS-8-EC-78-2, MAY 1978
 ABST THIS REPORT SUMMARIZES NICHOL'S OBSERVATIONS ON THE ENVIRONMENTAL DAMAGE AND THE CLEANUP EFFORTS RESULTING FROM THIS CATASTROPHIC SPILL.
 KEYS CLEAN-UP, ENVIRONMENTAL EFFECTS, TECHNIQUES AND SYSTEMS
 CODE 71527
- AUTH NIEMAN L.D., CLINE M.C., WOODFORD C.R.
 TITLE DESIGN OF A REFINERY BOOM TO PREVENT OIL SPILLS
 PUBL SHELL OIL CO. 1973 CONFERENCE
 ABST THIS MODERN BOOM OPERATED BY SHELL OIL CO. AS PART OF THE WYON RIVER REFINERY IN ILL. WAS DESIGNED TO INCLUDE FEATURES WHICH MINIMIZE THE POSSIBILITY OF OIL SPILLS.
 CODE 81114
- AUTH NIGHTINGALE J., NICHOLS J.A.
 TITLE BEACH PROTECTION: SHELL OIL HEADER CHEMICAL WARREN SPRING LABORATORY, LB 104101, 1973
 ABST THIS REPORT COVERS BRIEFLY THE ASSESSMENT OF A CHEMICAL PRODUCT, SHELL OIL HEADER, WHICH CAN BE USED TO PROTECT BEACHES FROM OIL WASHED ASHORE.
 KEYS SHELL OIL HEADER, PROTECTION, PREVENTION, CLEANUP
 CODE 29204
- AUTH NINOUJ C.J.
 TITLE A SIMPLE MODEL OF ENTRAINMENT AND TURBULENT DIFFUSION ACROSS A DENSITY INTERFACE IN THE OCEAN
 PUBL JOURNAL OF THE SCIENTIFIC SOCIETY OF BRUSSELS, VOL. 64, NO. 111, 1972
 ABST THE AIM OF THE PRESENT STUDY IS THE INTERPRETING
- OF AN INSITU EXPERIMENT MADE BY MOODS IN THE MEDITERRANEAN OFF MALTA (MCCDS 1966).
 KEYS DENSITY, SPREAD, ENTRAINMENT
 CODE 63247
- AUTH NISLER P., GOLDBSTEIN M.
 TITLE NON-CHEMICAL MODEL FOR PREDICTION OF SURFACE CURRENTS IN THE OCEAN
 PUBL USCC, OFFICE OF RESEARCH AND DEVELOPMENT, REPORT NO. CU-D-40-75, MAY 1974
 CODE 07139
- AUTH NIXON R.W.
 TITLE DELEGATION FUNCTIONS UNDER THE FEDERAL WATER POLLUTION CONTROL ACT
 PUBL OFFICE OF THE PRESIDENT FEDERAL REGISTER, 35:11477, 1972
 CODE 11114
- AUTH NODA REPORT
 TITLE PRELIMINARY SCIENTIFIC REPORT, THE ARGO MERCHANT OIL SPILL
 PUBL NODA REPORT, MARCH 1977
 ABST THIS REPORT DISCUSSES THE SCIENTIFIC ACTIVITY AIMED AT DESCRIBING THE MOVEMENT AND FATE OF OIL RELEASED BY THE TANKER AS A STEP IN ASSESSING THE ECOTOXICAL EFFECTS OF THE SPILL.
 KEYS PHYSICAL-CHEMICAL MOVEMENT OF OIL, ECOLOGISTS, PHYSICAL-CHEMICAL, BIOLOGICAL PROCESSES
 CODE 05749
- AUTH NOLL C.
 TITLE EVAPORATION AND DISSOLUTION OF OIL SPILLS
 PUBL OCEAN ENGINEERING DEPT., UMI, AUG. 1977
 ABST THIS PAPER DISCUSSES THE FIRST CHANGES OF PETROLEUM SPILLED ON WATER - EVAPORATION, EVAPORATION, DISSOLUTION, WIND AND WATER ACTION
 KEYS EVAPORATION, DISSOLUTION, WIND AND WATER ACTION
 CODE 65897
- AUTH NOLL C.J.
 TITLE A PREDICTIVE MODEL ON THE SPREAD AND TRANSPORT OF OIL SPILLS. M.S. THESIS (ROUGH DRAFT)
 PUBL MONTREAL-LIMITED - CANADA
 ABST SPREADING OF OIL CAN VARY GREATLY DEPENDING UPON THE PHYSICAL AND CHEMICAL CHARACTERISTICS (I.E., VISCOSITY, SURFACE TENSION, SURFACE ACTIVE AGENTS, ETC.) OF THE OIL AND THOSE OF THE SURROUNDING ENVIRONMENT.
 KEYS VISCOSITY, SURFACE TENSION, OIL SPILL
 CODE 77487
- AUTH NOLL C.J., SPAULDING R.L.
 TITLE APPLICATION OF AN OIL SPILL COMPUTER MODEL TO MARRAGANSETT BAY AND RHODE ISLAND SOUND
 PUBL DEPT. OF OCEAN ENGINEERING, UMI
 ABST TWO MODELS HAVE BEEN DEVELOPED. A LONG TERM MODEL WHICH PREDICTS SURFACE DRIFT ONLY OVER A TIME PERIOD ON THE ORDER OF DAYS. THE SECOND MODEL, A SHORT TERM MODEL, WITH REAL TIME CAPABILITIES IS MORE COMPLEX AND INCLUDES ESTIMATIONS OF SPREADING, DRIFT, OIL DENSITY CHANGES, AND EVAPORATION AND DISSOLUTION OF OIL OVER A TIME PERIOD ON THE ORDER OF HOURS. THE MODELS ARE USED TO SIMULATE ACTUAL AND HYPOTHETICAL SPILLS IN RHODE ISLAND SOUND AND MARRAGANSETT BAY.
 KEYS CONTINGENCY, CLEANUP, COMPUTER MODEL, SPREADING, DRIFTING
 CODE 76617
- AUTH NORTON R.B., LEACH D.
 TITLE AN OIL RECOVERY SYSTEM FOR SAN FRANCISCO BAY AREA
 PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
 ABST THIS PAPER DESCRIBES IN DETAIL THE PERFORMANCE SPECIFICATION FOR THE RECOVERY SYSTEMS.
 KEYS RECOVERY, WAVE TANK PREDICTIONS, REQUIREMENTS FOR TANK VESSEL CERTIFICATION
 CODE 85077
- AUTH NOTTAT H.
 TITLE LONG TERM EFFECTS OF AN OIL SPILL ON PUCUS MACEDEA IN A SMALL BALTIC BAY
 PUBL JOURNAL OF THE FISHERIES, VOL. 39, NO. 9, MAY 1978
 ABST LONG TERM EFFECTS OF AN OIL SPILL OCT. 4, 1970, THE SMALL TANKER IRINI RAN AGROUND IN THE SOUTHERN PART OF THE STOCKHOLM ARCHIPELAGO, RELEASING ABOUT 1000 TONS OF MEDIUM AND HEAVY FUEL OIL.
 KEYS ALGAE, LITTORAL COMMUNITY, TANKER IRINI
 CODE 26697
- AUTH O'BRIEN J.A.
 TITLE OIL SPREADING ON WATER FROM A STATIONARY LEAKING SOURCE
 PUBL CHEM. ENG. NO. 224 1970
 CODE 20434
- AUTH O'BRIEN J.A.
 TITLE WIND TUNNEL EXP. ON OIL SLICK TRANSPORT
 PUBL J. OF HYDRAULIC RESEARCH, VOL. 8, 1971
 CODE 20446
- AUTH O'BRIEN V.
 TITLE UNSTEADY CAVITY FLOWS: OSCILLATORY FLAT ODE FLOWS
 PUBL 65th PUB.
 ABST THE OSCILLATORY CAVITY FLOWS REPORTED HERE ARE EXTENSIONS OF PREVIOUSLY STUDIED STEADY CLOSED

- ABSTRACT**
CODE RECTANGULAR CAVITY FLOWS CROSS FLOWS.
 27024
- AUTH** ODA A.
TITLE EVALUATION OF POLYCOMPLEX 4-11 AS AN OIL DISPERSANT
- PUBL** THE ONTARIO WATER RESOURCES COMMISSION, DIVISION OF RESEARCH, PAPER NO. 2020, JUNE 1968
- ABST** THIS PAPER DISCUSSES THE EFFECTIVENESS OF POLYCOMPLEX 4-11 AS A DISPERSANT.
- KEYW** DISPERSANTS, EMULSIFIER, BIOLOGICAL TREATABILITY
- CODE** 2137F
- AUTH** ODA A.
TITLE LABORATORY EVALUATION OF CHEMICAL OIL DISPERSANTS
- PUBL** ONTARIO WATER RESOURCES COMMISSION
- ABST** THIS PAPER DISCUSSES SOME OF THE METHODS WHICH CAN BE USED TO EVALUATE CHEMICAL OIL DISPERSANTS IN ORDER TO OBTAIN SOME PRELIMINARY DATA RELATED TO THEIR EFFECTIVENESS AS DISPERSANTS AND PROBLEMS THAT MAY RESULT FROM THEIR USE.
- KEYW** CHEMICAL OIL DISPERSANTS, EFFECTIVENESS, PROBLEMS
- CODE** 2150A
- AUTH** OFFSHORE OIL TASK GROUP
TITLE SUMMARY THE GEORGES BANK PETROLEUM STUDY, VOL. 1 AND 11
- PUBL** N.I.L., SEA GRANT PROJECT OFFICE, FEB. 1, 1973
- ABST** VOLUME 1 AND VOLUME 11 OF A THREE VOLUME REPORT STUDYING THE IMPLICATIONS OF A PETROLEUM DEVELOPMENT ON THE NEW ENGLAND CONTINENTAL SHELF.
- KEYW** REGIONAL ECONOMY, PETROLEUM DISCOVERY, ENVIRONMENTAL QUALITY, DISCHARGES, SPILLS
- CODE** 0573F
- AUTH** OFFSHORE OIL TASK GROUP
TITLE THE COMPARATIVE TOXICITIES OF CRUDE OIL: THE ECOLOGICAL EFFECTS OF OIL POLLUTION ON LITTORAL COMMUNITIES
- PUBL** INST. PETROL., LONDON, 172-180
- CODE** 1091F
- AUTH** OIL AND HAZARDOUS MATERIALS RESEARCH SECTION
TITLE OIL SKIMMING EQUIPMENT
- PUBL** U.S. DEPARTMENT OF THE INTERIOR, FEDERAL WATER QUALITY ADMINISTRATION, MAY 1970
- ABST** OIL SKIMMING DEVICES ARE USED TO PHYSICALLY RECOVER OIL FROM THE WATER SURFACE.
- KEYW** OIL SKIMMING DEVICES, SKIMMERS, OIL RECOVERY DEVICES, REMOVAL
- CODE** 0964F
- AUTH** OPPENHEIMER E.
TITLE MICROBIOLOGICAL SEEDING TO ACCELERATE DEGRADATION OF HYDROCARBONS
- PUBL** UNIV. OF TEXAS, FOR EPA, NO. 15080HW, 7721545, SSIF NO. GHA 1643-1
- CODE** 0471B
- AUTH** OSA C.
TITLE THE ELECTRICAL PROCESS IN THE BREAKING OF DILUTE OIL-IN-WATER EMULSIONS
- PUBL** OFFICE OF WATER RESOURCES RESEARCH, JUNE 1974
- ABST** FILLS, GREASES, AND WAXES FREQUENTLY OCCUR IN INDUSTRIAL WASTE WATERS AS HEAVY DISPERSIVE COMPLEXES. INQUIRIES TO DETERMINE WHICH CHEMICAL AND WHAT QUANTITY OF THAT CHEMICAL NEEDED TO INDUCE A GIVEN EMULSION TO BREAK.
- KEYW** OIL GREASE AND WAX, WASTE WATERS, DISPERSIVE COMPLEXES, EMULSIONS
- CODE** 7531A
- AUTH** OTTO L.
TITLE ENVIRONMENTAL FACTORS IN OPERATIONS TO COMBAT OIL SPILLS
- PUBL** WORLD METEOROLOGICAL ORGANIZATION, WMO-359-845-9
- CODE** 0410A
- AUTH** OTTO L.
TITLE OROGRAPHIC ASPECTS OF OIL POLLUTION
- PUBL** METEOROL. TECHN. T., VOL. 1, 1972
- CODE** 2367H
- AUTH** OFFFIELD J.L.
TITLE DEVELOPMENT OF A NON-TOXIC SIMULATED OIL FOR MARINE TESTING PROGRAMS
- PUBL** OTC PAPER NO. OTC 1524, OFFSHORE TECHNOLOGY CONFERENCE, MAY 1972
- CODE** 0647F
- AUTH** ORVATHO E.B., BRACKEN J., RASLER J.L.
TITLE APPLICATION OF GLASS CAPILLARY COLUMNS TO MONITOR PETROLEUM-TYPE HYDROCARBONS IN MARINE SEDIMENTS
- PUBL** JOURNAL OF CHROMATOGRAPHIC SCIENCE, VOLUME 15, MAY 1977
- ABST** HIGH RESOLUTION GLASS CAPILLARY COLUMNS COATED WITH SI 52 LIQUID PHASE WERE USED TO RESOLVE THE INDIVIDUAL HYDROCARBONS EXTRACTED FROM SEDIMENT SAMPLES COLLECTED FROM THREE OFFSHORE CONTINENTAL SHELF AREAS.
- CODE** 7705 F
- AUTH** OREN B.W.
TITLE SMALL-SCALE HORIZONTAL VORTICES IN THE SURFACE LAYER OF THE SEA
- PUBL** JOURNAL OF MARINE RESEARCH, VOL. 24, 1966
- ABST** A VORTICE SYSTEM IN THE WATER NEAR THE SEA SURFACE HAS BEEN INFERRED FROM COLLECTION INTO PARALLEL ROWS OF A POSITIVELY PHOTOGRAPHIC ZOOPLANKTON POPULATION.
- KEYW** VORTICE SYSTEM, WATER VELOCITY, CONVERGENCE PLANES
- CODE** 6560F
- AUTH** OWENS E. LESLIE J.
TITLE COASTAL ENVIRONMENTS OF CANADA: THE IMPACT AND CLEAN-UP OF OIL SPILLS
- PUBL** RESEARCH AND DEVELOPMENT DIVISION, ENVIRONMENTAL EMERGENCY BRANCH, EPS-3-EC-77-13, APRIL 1977
- ABST** A REVIEW OF THE SHORELINE AND PROCESS CHARACTERISTICS OF CANADA'S COASTS INVOLVED DEFINITION AND DESCRIPTION OF 24 COASTAL ENVIRONMENTS AND SHOWS THAT LITTORAL PROCESSES OPERATE AT RELATIVELY LOW-ENERGY LEVELS IN MANY REGIONS DUE TO THE SMALL FETCH AREAS ON MOST COASTS AND THE SIGNIFICANT ROLE OF ICE IN ALL LITTORAL ENVIRONMENTS, EXCEPT FOR THE BRITISH COLUMBIA AND SOUTHERN NOVA SCOTIA COASTS.
- KEYW** COASTAL ENVIRONMENTS, FETCH, ICE ROLES
- CODE** 7184F
- AUTH** OWENS E.M.
TITLE MECHANICAL DISPERSAL OF OIL STRANDED IN THE LITTORAL ZONE
- PUBL** JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1970
- ABST** THIS REVIEW OF THE CONCEPTS ASSOCIATED WITH LITTORAL PROCESSES, IN TERMS OF THE MECHANICAL DISPERSAL OF STRANDED OIL, PROVIDES THE BASIS FOR ESTIMATION OF THE PERSISTENCE OF OIL ON SHORELINES.
- KEYW** WEATHERING, DISPERSAL OF PETROLEUM, COASTAL PROCESSES, WAVE ENERGY, SEA ICE
- CODE** 2607F
- AUTH** OWENS E.M. LESLIE J.
TITLE COASTAL ENVIRONMENTS, OIL SPILLS AND CLEAN-UP PROGRAMS IN THE BAY OF FUNDY
- PUBL** EPA, ATLANTIC REGION, EPS-3-EC-77-5, FEB. 1977
- ABST** GUIDELINES AND RECOMMENDATIONS FOR PROTECTION AND CLEANUP OF THE SHORES OF THE BAY OF FUNDY ARE PRESENTED AND ARE RELATED TO THE NATURE OF THE SHORELINE, THE SEDIMENTS, THE SHORELINE PROCESSES AND THE EFFECTIVENESS OF AVAILABLE TECHNIQUES.
- KEYW** COASTAL FEATURES, SHORELINE PROCESSES, IMPACT AND PERSISTENCE
- CODE** 7166F
- AUTH** REEDMAN J.P.
TITLE A STUDY OF THE PERFORMANCE CHARACTERISTICS OF THE OLEOPHILIC BELT "OIL SCRUBBER"
- PUBL** PHYSICAL REVIEW
- ABST** THIS PAPER DISCUSSES THE PERFORMANCE OF THE "OIL SCRUBBER". THE STABILITY OF THE BELT IS A PRIMARY CONCERN FOR OPERATIONS IN THE PRESENCE OF TRANSVERSE CURRENTS.
- KEYW** REMOVAL, RECOVERY RATE, EFFICIENCY
- CODE** 0620F
- AUTH** OREN B.W.
TITLE OCEAN POLLUTION: WHAT CAN THE LAB OF THE SEA CONFERENCE DO?
- PUBL** LAB OF THE SEA: THE ENERGY REGIME OF THE OCEANS, GALLAGHER PUBLISHING, CO. 1974
- ABST** REGARDS THE STANDARDS SET UP FOR RESEARCH AND MONITORING FOR STRONGER RULES AND REGULATIONS GUARDING THE SEA.
- CODE** 3104A
- AUTH** PACIFIC NORTHWEST LABORATORIES
TITLE RECOVERY OF OIL SPILLS USING WIND ASSISTED AIRLIFT SYSTEM
- PUBL** EPA, WATER QUALITY OFFICE, WATER POLLUTION CONTROL RESEARCH SERIES, JULY 1970
- ABST** STUDIES WERE CONDUCTED TO DETERMINE THE FEASIBILITY OF A CONCEPT FOR RECOVERY OF FLOATING OIL SLICERS WHICH UTILIZES A PUMP INDUCED WIND AND A VACUUM SUCTION OF CANADA NOZZLE.
- KEYW** WIND, CANADA NOZZLE, WAVE SUPPRESSOR
- CODE** 0567F
- AUTH** PAL D.
TITLE THE COANDA-EFFECT OIL-WATER SEPARATOR: A FEASIBILITY STUDY
- PUBL** NAVAL UNDERWATER SYSTEMS CENTER, WASHINGTON, DC, REPORT NO. W-1391, FEB. 1974
- ABST** AN EXPERIMENTAL INVESTIGATION WHICH ESTABLISHES THE FEASIBILITY OF USING THE COANDA EFFECT IN DEVELOPING AN OIL WATER SEPARATOR IS DESCRIBED. FLUID DYNAMIC PHENOMENA, "WALL ATTACHMENT"
- CODE** 0513F
- AUTH** PANKOVIC B.J.
TITLE COMPOSITIONAL DATA ON API REFERENCE OILS USED IN BIOLOGICAL STUDIES: A NO. 7 FUEL OIL, A BUNKER C, BUNKER CRUDE OIL AND SOUTH LOUISIANA CRUDE OIL
- PUBL** API, REPORT NO. RD 84 76, FEB. 27, 1974
- ABST** AN ANALYSIS OF FOUR OILS, MOST OF THESE METHODS ARE FAIRLY STANDARD IN THE PETROLEUM INDUSTRY AND THE IN DESCRIPTION IS INCLUDED AS A GUIDE TO SHOW ONE OF THE RESEARCH AND ENGINEERING HAS MADE CHANGES AND MODIFICATIONS TO EXISTING PROCEDURES. SAMPLING, OIL IN THE ENVIRONMENT, REFERENCE OILS
- KEYW** CODE 0537F

- AUTH PANICHERY R.J., BROWN R.A.
 TITLE ANALYTICAL METHODS FOR POLYNUCLEAR AROMATIC HYDROCARBONS IN CRUDE OILS, HEATING OILS, AND MARINE TISSUES
 PUBL ENVIRONMENTAL AND ENGINEERING CO., ANALYTICAL AND INFORMATION DIV., FOR EPA 1975 CONFERENCE
 REFS ANALYTICAL METHODS, POLYNUCLEAR AROMATIC HYDROCARBONS, MARINE TISSUES
 CODE 00829
- AUTH PANICHERY R.
 TITLE OFFSHORE DRILLING: FISHERMAN AND OILMAN CLASH IN ALASKA
 PUBL SCIENCE VOL. 104,
 ABST HIGHLIGHTS EFFORTS BY A GROUP OF ALASKAN FISHERMEN - PROCESS AND ATTEMPTS TO INVALIDATE A STATE OFFSHORE LEASE.
 REFS OFFSHORE LEASES, LEGISLATION
 CODE 90427
- AUTH PARADUST R.J.
 TITLE COAST GUARD ANTI-POLLUTION ENGINEERING
 PUBL THE MILITARY ENGINEER, NO. 421, SP1-OCT, 1977
 ABST A DISCUSSION OF THE DUTIES OF THE COAST GUARD AS PERTAINING TO OIL SPILLS AND POLLUTION ON THE OCEAN.
 CODE 60769
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 REYN OIL SPILL MOTION, OIL SPILL DRIFT, WIND AND CURRENTS
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- AUTH PRINCE J.S., BROWN G.A.
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 ABST TO CHARACTERIZE THE OIL SPILL REPORT DATA FOR THE PERIOD FROM 1967 TO 1971, TO APPLY THE INFORMATION TO A NEW OIL CONTINGENCY PLAN FOR COASTAL AND WIND WATERS, FOUR IMPORTANT CATEGORIES WERE DEVELOPED FOR ADDITIONAL DATA SUMMARY AND OIL SPILL CONTINGENCY PLANNING: 1. SOURCE OF SPILL 2. PATH TO ESTUARY 3. NOTIFICATION OF SPILL 4. RESPONSE TO SPILL
 KEYW CONTINGENCY, ESTUARY, SOURCE, RESPONSE
 CODF 0031P
- AUTH PRINCE J.S., BROWN G.A.
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 KEYW CONTINGENCY, EQUIPMENT, RESOURCES
 CODF 0032P
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 KEYW SPILL, PATH TO ESTUARY, NOTIFICATION, RESPONSE, CONTINGENCY
 CODF 0127P
- AUTH PRICE R.S., WAGY G.T., CONWAY E.R.A.
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- AUTH PRISTON S.P.
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 KEYW MICROBIAL DEGRADATION, TURBULENCE, HYDROCARBON LAYERS
 CODF 1066P
- AUTH PROBSTEN P., DELICHAITSINS M.A.
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 PUBL INT. J. NUM. ANAL. 1974
 ABST THE PRESENT STUDY IS AN ATTEMPT TO OBTAIN A BETTER UNDERSTANDING OF HOW DISPERSED COLLOIDAL PARTICLES COAGULATE INTO LARGER SIZE FLOWS UNDER THE ACTION OF A TURBULENT FLOW.
 KEYW DISPERSED COLLOIDAL PARTICLES, COAGULATION, TURBULENT FLOW
 CODF 1138P
- AUTH PRONE A. C.
 TITLE REMOTE SENSING OF OIL POLLUTION AT THE SEA SURFACE BY DIRMING OF WATER WAVES BY AN OIL LAYER AS A POSSIBLE INDICATOR FOR SLAP OBSERVATIONS
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 KEYW WATER WAVES, OIL POLLUTION, DETECTION
 CODF 1120 P
- AUTH PUTMAN B.A.
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 KEYW PARTICLE CONCENTRATION, IONIC STRENGTH, BUBBLE DEPTH RELEASE
 CODF 0304P
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 KEYW BIODEGRADATION
 CODF 5020P
- AUTH RAJ P.R.
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 KEYW SEASTATE, BREAKING WAVES, TURBULENCE
 CODF 2050P
- AUTH RANSTEP R.C.
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- AUTH RAPHALIAN L.A., HARRISON R.
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 KEYW ACTIVATED SLUDGE, ENERGY CONVERSION, ENVIRONMENTAL ENGINEERING
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- AUTH RAY S.S., STRIPS R.L., TOMJANOVICH D.A.
 TITLE A STATE OF THE ART REPORT ON INTAKE TECHNOLOGIES
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- AUTH RAYMOND G.S., HAYES J.V., OGDEN E.C.
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- AUTH REED R.
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 CODF 1777P
- AUTH REIFER M.G., CORWELL E.B.
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- AS STRESSES THAT OYFORM AND TRANSFORM COMMUNITY
STRUCTURE AND REVERSE THE USUAL SEQUENCE OF
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ECOSYSTEM, POLLUTION
- KEYW
CODE 7737F
- AUTH REHMOLD R., LASKO L., SHAW C., WERNOWSKI E.
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- ABST THE PURPOSE OF THIS RESEARCH WAS TO DETERMINE THE
MEDIAN TOXICITY OF NO. 2 AND NO. 6 OILS TO
REPRESENTATIVE FISH SPECIES AND IN ADDITION
DETERMINE THE EFFECT OF A DISPERSANT AND
COLLECTING AGENT ON THIS TOXICITY.
- KEYW DISPERSANTS, COLLECTING AGENTS, TOXICITY
- KEYW
CODE 2144F
- AUTH REIF G.W., STEPHAN L.E.
TITLE EVALUATION OF WASTE WATERS FROM PETROLEUM AND COAL
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- PUBL EPA, WASH. DC, 72-77-001, DEC. 1972
- ABST AN EVALUATION ON POLLUTION PROBLEMS, ABATEMENT
TECHNIQUES AND CONTROL TECHNIQUES RELEVANT TO THE
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- KEYW ABATEMENT, CONTROL TECHNIQUES, PETROLEUM AND COAL
INDUSTRIES
- CODE 6068F
- AUTH REISIG P.
TITLE FINAL REPORT - OIL SPILL DRIFT CAUSED BY THE
COUPLED EFFECTS OF WIND AND WAVES
- PUBL DEPT. OF TRANSPORTATION, USCG, OCT. 1973
- ABST THE RESULTS IN THIS INVESTIGATION SHOW THAT WAVE
EFFECTS ARE COMPLICATED BY WIND EFFECTS IN A
COMPLICATED MANNER AND NEGLECTING THE WAVES CAN
LEAD TO SERIOUS ERRORS.
- KEYW WAVE EFFECTS, WIND EFFECTS, OIL SPILL DRIFT
- KEYW
CODE 7546F
- AUTH REISIG P.
TITLE MEASUREMENT OF OIL SPILL DRIFT CAUSED BY THE
COUPLED PARALLEL EFFECTS OF WIND AND WAVES
- PUBL MAR. SOC. SCI. SER. 1, VOL. 6, 1974
- CODE 2048F
- AUTH REISIG P.
TITLE OIL SPILL DRIFT CAUSED BY THE COUPLED EFFECTS OF
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- PUBL 1973
- ABST THIS YEAR STUDY OF THE POTENTIAL EFFECT OF WIND AND
WAVES ON OIL WAS INITIATED TO EVALUATE THE
IMPORTANCE OF COUPLED WIND AND WAVE DRIFT
MECHANISM COMPUTER SIMULATION OF THE TOTAL DRIFT
POTENTIAL EFFECT, WIND AND WAVES, OIL SPILL DRIFT
- KEYW
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- AUTH REISH D.J.
TITLE A CRITICAL REVIEW OF THE USE OF MARINE
INVERTEBRATES AS INDICATORS OF VARYING DEGREE OF
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- PUBL P.A.C. TECHNICAL CONFERENCE ON MAR. POLLUTION AND
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- CODE 1049F
- AUTH RENZI G.
TITLE IMPACT OF CRUDE OIL, DERIVATIVES AND
DISPERSANTS ON LARVAE
- PUBL MARINE POLLUT. BULL. 610-13, 1970
- CODE 5032F
- AUTH RICCI R.J., BRANDE H.J.
TITLE DEVELOPMENT IN FRANCE OF AN OFFSHORE OIL SPILL
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- PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2702,
MAY 4-8, 1975
- ABST A DESCRIPTION OF THESE OPERATIONS AND SUMMARY OF
THE RESULTS ARE PRESENTED.
- KEYW SKIMMER, CLEANUP, CONTAINMENT, COLLECTION,
PUMPING, STORAGE TRANSFER
- CODE 0550F
- AUTH RICE S.D., WILES D.A., SHORT J.W.
TITLE THE EFFECT OF PRUDHOE BAY CRUDE OIL ON SURVIVAL
AND GROWTH OF EGGS, ALEVINS, AND PRY OF PINK
SALMON, ONCOMMENSUS GORBUSCHA
IN THE PRUDHOE BAY FISHERIES LAB., WASH. DC, FOR EPA
1974 CONFERENCE
- KEYW PRUDHOE BAY CRUDE OIL, SURVIVAL, PINK SALMON
- KEYW
CODE 0141F
- AUTH RICHARDSON P.L., WASTAND A.
TITLE GULF STREAM CYCLONIC RINGS
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- ABST THIS PAPER DISCUSSES A STUDY ON EFFECTS OF
CYCLONIC RINGS GENERATED BY THE GULF STREAM.
CYCLONIC RINGS, GULF STREAM, MESOSCALE OCEANIC
FEATURES
- KEYW
CODE 0570F
- AUTH RICHARDSON P.S.
TITLE DEVELOPMENT OF A SYSTEM FOR MEASUREMENT OF SURFACE
CURRENTS AND OCEANIC CURRENT OBSERVATIONS
- PUBL NOVIA UNIV. AD 707787, USCG 8 10-75
- CODE 0407F
- AUTH RICHARDSON P.S., COMPTON F.
TITLE PETROLEUM SPILLAGE, MOINES - FAIRBANKS MILITARY
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- PUBL ARMY RESEARCH OFFICE, LIFE SCIENCES DIV., D A
PROJECT TAGC1130710, APRIL 1972
- ABST PRELIMINARY INVESTIGATION OF PETROLEUM SPILLAGE
- KEYW
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- AUTH RIDWAY R.W.
TITLE INSPECTION OF DRIFT OF SURFACE OIL WITH WIND AND
TIDE
- PUBL W.J. JI. PAR. FRESHWATER RES. VOL. 6, 1972
- CODE 2049F
- AUTH RISENHOUGH R.W.
TITLE POLLUTANTS IN MARINE MAMMALS, A LITERATURE REVIEW
AND RECOMMENDATIONS FOR RESEARCH
- PUBL MARINE MAMMAL COMMISSION
- ABST A REVIEW OF THE PUBLISHED LITERATURE AND OF
SELECTED UNPUBLISHED DATA ON THE DISTRIBUTIONS AND
CONCENTRATIONS OF POLLUTANTS IN MARINE MAMMALS HAS
SHOWN THAT ALL MARINE MAMMAL POPULATIONS ARE NOW
EXPOSED TO A CERTAIN LEVEL OF ANTHROPOGENIC
CHEMICALS.
- KEYW MARINE MAMMALS, MARINE POLLUTION
- KEYW
CODE 7706F
- AUTH RIZLEY C.
TITLE AIR MODULATED VACUUM OIL RECOVERY COLLECTION OF
SPILLED OIL (RAGS)
- PUBL EPA, WASH. DC, 72-033, 873-0571, AUG. 1973
- ABST AN AIR MODULATED VACUUM OIL RECOVERY TECHNIQUE HAS
BEEN DEVELOPED IN AN EXPERIMENTAL AND ENGINEERING
DESIGN PROJECT AS A METHOD OF COLLECTING OIL
SPILLED ON WATER.
- KEYW AIR MODULATED VACUUM, RECOVERY TECHNIQUE,
COLLECTING OIL
- KEYW
CODE 0067F
- AUTH RITCHIE J.E., ALLEN F.J.
TITLE PETROLEUM SYSTEMS RELIABILITY ANALYSIS, A PROGRAM
FOR PREVENTION OF OIL SPILLS USING AN AGP
APPROACH TO A STUDY OF OFFSHORE AND ONSHORE CRUDE
OIL PETROLEUM SYSTEMS
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WATER PROGRAM OPERATIONS
- ABST THE ANALYSIS FURNISHED IN DETAIL THE CAUSES OF
POLLUTING SPILLS FROM SELECTED PET. SYSTEMS
ONSHORE AND OFFSHORE CRUDE OIL DRILLING PRODUCTION
AND GATHERING/DISTRIBUTION SYSTEMS. THE STUDY
INCLUDES THE COMPILATION OF DATA FROM FEDERAL,
STATE AND INDUSTRIAL SPILL REPORTS, A FIELD SURVEY
OF THE VARIOUS TYPES OF FACILITIES AND AN ANALYSIS
OF SPILL-CAUSING FAILURES.
- KEYW
CODE 0023F
- AUTH ROTHMAN S., WALKER D., AND CROSS R.
TITLE STEADY-STATE BOOMWELL FOR OIL BARRIERS
- PUBL FEDERAL WATER POLLUTION CONTROL ADMINISTRATION
CONTRACT W-143001
- ABST FOR THE RATIONAL DESIGN OF AN OIL SLICK
CONTAINMENT AND COLLECTION SYSTEM, THE BEHAVIOR OF
AN OIL SLICK HELD AGAINST A SURFACE BARRIER BY A
STEADY CURRENT MUST BE KNOWN. DERIVATIONS FOR
CALCULATING THIS QUANTITY ARE SHOWN.
- KEYW
CODE 3052F
- AUTH ROBBINS R.J.
TITLE THE OIL BOOM IN A CURRENT
- PUBL P.I.T., JUNE 1970
- ABST AN INVESTIGATION OF THE SIMPLEST REALISTIC CASE
I.E. A BARRIER HOLDING OIL IN A STEADY CURRENT
WITH NO SURFACE WAVES OF WIND.
- KEYW
CODE 0010F
- AUTH ROBERTS A.E.
TITLE SHORE TERMINATION FOR OIL SPILL BOOMS
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- CODE 0066F
- AUTH ROBERTS A.E.
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- AUTH ROBINCHAUF T.J., NUGENT M.
TITLE CHEMICAL ENHANCEMENT OF THE BIO-DEGRADATION OF OIL
POLLUTION
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APR. 19-21, 1971, JOURNAL OF PETROLEUM TECHNOLOGY,
JAN. 1972
- ABST IN THIS PAPER THE RESULTS OF A STUDY OF THE
EFFECTS OF CHEMICAL DISPERSING AGENTS ON THE RATE
OF MICROBIAL DESTRUCTION OF CRUDE OIL IN AQUEOUS
ENVIRONMENTS ARE DESCRIBED.
- KEYW DISPERSANTS, BIODEGRADATION, MICROBIAL DESTRUCTION
- KEYW
CODE 0052F
- AUTH ROBINSON A.J.
TITLE ASSESSMENT OF DEVICES FOR THE REMOVAL OF OIL FROM
ONSHORE AND INLAND WATERS
- PUBL DEPT. OF TRADE AND INDUSTRY, SSIEI NO. 000-730

- CODE 0354A
- AUTH ROBINSON A.J.
 TITLE STUDY AND ASSESSMENT OF DEVICES FOR RECOVERY OF OIL AT SEA
 PUBL DEPT. OF TRADE AND INDUSTRY, SSIC NO. 1 600-742
 CODE 0357A
- AUTH ROBINSON A.J.
 TITLE STUDY AND ASSESSMENT OF EQUIPMENT FOR CONTAINMENT OF OIL AT SEA
 PUBL DEPT. OF TRADE AND INDUSTRY, SSIC: 600-744
 CODE 0354A
- AUTH ROBINSON J.
 TITLE A PRACTICAL OIL SPILL CONTROL TRAINING SCHOOL
 PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
 ABST THIS PAPER DESCRIBES A PRACTICAL OIL SPILL TRAINING COURSE OFFERED BY TEXAS ENGINEERING EXTENSION SERVICE, TEXAS A AND M UNIVERSITY BEGINNING MARCH, 1975.
 KEYW PREVENTION, CONTROL, TRAINING COURSES
 CODE 0010F
- AUTH RUDENBERGER C.A.
 TITLE A SYSTEMS EGR. SOLUTION FOR OCEAN SEA OIL SPILLS
 PUBL JOURNAL OF HYDRODYNAMICS, 6144, VOL. 9, 1971
 CODE 0737A
- AUTH RODRIGUEZ S., WEBSTER E., LEARY J.
 TITLE THE FREE VORTEX APPROACH TO RECOVERY OF FLOATING OIL
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1908, MAY 4-8, 1974
 ABST RECENT RESULTS OF DEVELOPMENT AND TESTING OF THE FREE VORTEX APPROACH TO FLOATING OIL RECOVERY ARE PRESENTED.
 KEYW HIGH SEAS OIL SPILL RECOVERY, FREE VORTEX, SEAWING
 CODE 0074F
- AUTH ROUSSEAU G.J., ANDERSON N., BLAYLOCK J.W.
 TITLE UPTAKE OF HYDROCARBONS FROM MARINE SEDIMENTS CONTAMINATED WITH PUDDOUE BAY CRUDE OIL: INFLUENCE OF FEEDING TYPE OF TEST SPECIES AND AVAILABILITY OF POLYCYCLIC AROMATIC HYDROCARBONS
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 9, MAY 1970
 ABST SPECIFIED BENTHIC ANIMALS WERE EXPOSED TO MARINE SEDIMENTS CONTAMINATED WITH PUDDOUE BAY CRUDE OIL, AND UPTAKE OF HYDROCARBONS WAS MONITORED UNDER VARIOUS EXPERIMENTAL SCHEMES.
 KEYW HYDROCARBONS, SEDIMENTS, BIVALVE, SIPHONALID, FEEDING TYPE
 CODE 2069F
- AUTH ROGERS B., STEPHENSON T.
 TITLE OIL AND MARINE FISH: LOWYAT THE DEVELOPMENT OF CULTURE METHODS AND THE DETERMINATION OF CRUDE OIL EFFECTS ON THE EARLY LIFE STAGES OF SANDWICHES AND MICROGADUS
 PUBL PRE-PROPOSAL, EPA, URI GRADUATE SCHOOL OF OCEANOGRAPHY
 ABST BECAUSE OF THE VULNERABILITY TO POLLUTANTS, TELEOSTS ARE DESIRABLE TO USE FOR TESTING THE EFFECTS OF POLLUTANTS.
 KEYW TELEOSTS, MICROBIAL DEGRADATION, TOXICITY
 CODE 7055F
- AUTH ROYHOLM N., LARVE M.C., MARSHALL N., PAPPELL J.F.
 TITLE ECONOMIC IMPACT OF MARINE ORIENTED ACTIVITIES: A STUDY OF THE SOUTHERN NEW ENGLAND MARINE REGION
 PUBL URI, DEPT. OF FISH AND RESOURCE ECONOMICS, 1967
 KEYW ECONOMIC IMPACT, SOUTHERN NEW ENGLAND, MARINE ORIENTED ACTIVITIES
 CODE 0065F
- AUTH ROSEN A.
 TITLE THE FOUNDATIONS OF ORGANIC POLLUTANT ANALYSIS
 PUBL MUNICIPAL ENVIRONMENTAL RESEARCH LABORATORY, USEPA, 80747 309, DEC. 1970
 ABST THIS PAPER DESCRIBES A SYSTEMATIC ANALYSIS OF ORGANIC POLLUTANTS.
 KEYW ORGANIC POLLUTANTS, WATER SAMPLING, ANALYTIC METHODS, CARBON ADSORPTION
 CODE 3204F
- AUTH ROSS S.L.
 TITLE OIL SPILL TECHNOLOGY DEVELOPMENT IN CANADA
 PUBL CONFERENCE ON PREVENTION AND CONTROL OF OIL POLLUTION
 ABST IN THIS PAPER SOME OF THE RESEARCH AND TECHNOLOGY DEVELOPMENT PROJECTS TAKING PLACE IN CANADA, THE TECHNOLOGY DEVELOPMENT AND RESEARCH EFFORT IN CANADA HAS BEEN DIRECTED TOWARD COLO ENVIRONMENT PROBLEMS.
 KEYW CONTAINMENT, CLEANUP, CONTROL
 CODE 0515F
- AUTH ROSS S.L., PINGAS
 TITLE SPILL TECHNOLOGY NEWSLETTER
 PUBL RESEARCH AND DEVELOPMENT DIVISION, ENVIRONMENTAL PROTECTION AGENCY, ENVIRONMENTAL PROTECTION SERVICE, OTTAWA, ONTARIO
 CODE 2099B
- AUTH ROSS W.R.
 TITLE OIL POLLUTION AS AN INTERNATIONAL PROBLEM: A STUDY OF PUGET SOUND AND THE STRAITS OF GEORGIA
 PUBL UNIV. OF WASHINGTON PRESS, SEATTLE 1974
 ABST THROUGH THE AUTHOR'S CONCERN FOR THE OCEAN'S POLLUTION THIS BOOK LINES AT THE LEGISLATION ACTION TAKEN IN THE US AND CANADA TO REDUCE AND CONTROL OIL POLLUTION. IT ALSO DESCRIBES AND EVALUATES LEGISLATION IN THE US SINCE 1972
 KEYW OIL POLLUTION, PUGET SOUND LEGISLATION
 CODE 3079A
- AUTH ROSENTHAL M.
 TITLE THE GOVERNMENT AND THE OIL, CHEMICAL AND ATOMIC WORKERS UNION
 PUBL JOHN WILEY AND SON'S INC. NEW YORK, 1967
 ABST THE SCOPE OF THE STUDY IS LIMITED TO THE INTERNATIONAL UNION AND ITS ANALYSIS IS FOCUSED ON THE PRIMARY FUNCTIONS OF THE UNIONS. THE OIL IS COMPARED A WEA UNION.
 CODE 3084F
- AUTH RUBY C., HARD L., FISCHER J., BROWN J.
 TITLE BUZZARDS BAY OIL SPILL AN ARCTIC ANALOGUE
 PUBL COASTAL RESEARCH DIVISION, DEPT. OF GEOLOGY, UNIV. OF SO. CAROLINA
 ABST THIS PAPER ANALYZES THE INTERACTION OF THE ICE COVER WITH THE RATE AND FATE OF DISPOSAL OF THE SPILLED OIL. SPECIAL EMPHASIS WAS GIVEN PLACED ON AREAS OF OIL ACCUMULATION WITHIN THE ICE AND WAYS IN WHICH THE ICE COVERS TEND TO PROTECT THE SHORELINE FROM CONTAMINATION.
 KEYW CLEAN UP, CONTINGENCY, OIL ON ICE
 CODE 7051F
- AUTH RUCKENSTEIN E., CHI C.
 TITLE STABILITY OF MICROEMULSIONS
 PUBL UNKNOWN
 ABST A THERMODYNAMIC TREATMENT TO OBTAIN INFORMATION ON THE STABILITY OF MICROEMULSIONS AND THE SIZE OF THE DROPLETS IN STABLE MICROEMULSIONS IS PROPOSED.
 KEYW THERMODYNAMICS, MICROEMULSIONS, STABILITY
 CODE 6509F
- AUTH RUDDER C.L.
 TITLE AERIAL SURVEILLANCE SPILL PREVENTION SYSTEM
 PUBL EPA REPORT NO. 67-72-007
 CODE 2007F
- AUTH RUDDER C.L., REINHOLDF C.J., SPERRY J.L.
 TITLE SPILL PREVENTION SYSTEM
 PUBL CONTRACT NO. 60-01-0140, PROJECT NO. 150000A, AUG. 1972
 ABST AERIAL SURVEILLANCE SPILL PREVENTION SYSTEM.
 CODE 6072A
- AUTH RUDDER C.L., WALLACE S.C., REINHOLDF C.J.
 TITLE AERIAL DETECTION OF SPILL SOURCES
 PUBL OFFICE OF RESEARCH AND MONITORING, EPA
 ABST THE PURPOSE OF THE PROJECT WAS TO DEVELOP AN IMAGERY INTERPRETATION KEY FOR USE IN THE DETECTION AND IDENTIFICATION OF SPILL SOURCES TO INLAND OR COASTAL WATERWAYS FROM AERIAL PHOTOGRAPHS.
 CODE 6048F
- AUTH RUSSELL DONALD J.D.
 TITLE AN EXPERIMENTAL INVESTIGATION OF DRIFT PROFILES IN AN ESTUARINE CHANNEL
 PUBL HYDRAULICS RESEARCH STATION, WALLINGFORD, ENGLAND
 CODE 7067A 4
- AUTH RYAN W., ROSS S.L., WAGY F., SPRAGUE J.B.
 TITLE GUIDELINES ON THE USE AND ACCEPTABILITY OF OIL SPILL DISPERSANTS
 PUBL EPA
 CODE 5013A
- AUTH SACRETT W.R., ANDERSON J.W.
 TITLE PAST SPATIAL AND TEMPORAL DISTRIBUTION OF PETROLEUM DERIVED ORGANIC COMPOUNDS IN THE OCEAN AND THEIR SUBLETHAL EFFECTS ON MARINE ORGANISMS
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 CODE 0542A
- AUTH SALLA S.B.
 TITLE POSSIBLE SUGGESTION
 PUBL EIGHTH SESSION OF THE SUB-COMMITTEE ON MARINE POLLUTION, INCO HEADQUARTERS, LONDON, SEPT. 7-11, 1970
 ABST CONSIDERATION OF VARIOUS OIL INDUSTRIES OR ORGANIZATIONS SPONSORING THE DEVELOPMENT AND MAINTENANCE OF AN INTERNATIONAL CENTER FOR OIL SPILL TREATMENT
 KEYW COMPUTER FACILITY, COMMUNICATIONS NETWORK, DEVELOPMENT AND MAINTENANCE
 CODE 2036F
- AUTH SANDERS M.L.
 TITLE FLORIDA OIL SPILL IMPACT ON THE BUZZARDS BAY BENTHIC FAUNA: WEST PALMOUTH
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 9, MAY 1970
 ABST DISCUSSION OF BENEFITS AND SPECIES COMPOSITION IN OILED STATIONS.
 KEYW BENEFITS, HYDROCARBONS, INTENTIONAL CODE, LONG TERM EFFECTS, STATISTICS

- CODE 2649
 AUTH SANDERS M.L., GRASSIE J.P., HARRISON G.B.
 TITLE THE WEST PALM BEACH OIL SPILL. I. BIOLOGY
 PUBL AVAILABLE FROM NTIS AS PB-204 626, REPORT NO.
 NWO-72-27, APRIL 1972
 CODE 03349
- AUTH SARTON J.D., COUCH W.D., KAUFFMAN D.S.
 TITLE OIL SPILL CONTINGENCY PLANS FOR THE ALBERTA
 PIPELINE SYSTEMS
 PUBL EPA CONFERENCE 1975
 ABST PAPER INCLUDES: PIPELINE DRAINAGE CALCULATIONS,
 CONTINGENCY ORGANIZATION, ENVIRONMENTAL
 CONSIDERATIONS, IMMEDIATE RESPONSE ACTIONS, AND
 CONTINGENCY PLAN DEVELOPMENT
 KEYW CONTINGENCY PLAN, PIPELINE SYSTEMS, ENVIRONMENTAL
 CONSIDERATION
 CODE 01079
- AUTH SARTON J.D., FOGIT C.R., CASTLE R.B.
 TITLE OIL/SOLVENT HARVESTING SYSTEM FOR USE ON VESSELS
 OF OPPORTUNITY
 PUBL ENVIRON WATER QUALITY RESEARCH LAB., PREPARED FOR
 EPA, NC, 87-79-100, APR. 1975
 ABST A THREE-PHASE TEST PROGRAM WAS CONDUCTED TO
 EVALUATE CANDIDATE SYSTEM COMPONENTS AND OPERATING
 SPECIFICATIONS FOR THE OIL/SOLVENT HARVESTING
 SYSTEM.
 KEYW RECOVERY, OIL/SOLVENT HARVESTING SYSTEM, OIL ON
 WATER
 CODE 01945
- AUTH SARTON J.D., PAPP R.W.
 TITLE DRAG COEFFICIENTS OF SMALL, IRREGULAR PARTICLES
 THE BOUND CORRELATION: SANTA MONICA, CALIF.
 ABST THIS REPORT PRESENTS THE RESULTS OF SEVERAL
 LABORATORY TESTS CONDUCTED WITH SPHERICAL AND
 IRREGULARLY SHAPED PARTICLES. THESE MEASUREMENTS
 WERE MADE TO CLARIFY THE LAW OF FALL OF IRREGULAR
 PARTICLES IN THE RANGE OF REYNOLDS NUMBERS FROM
 0.05 TO 3.0. THE RESULTS OF THE EXPERIMENTS ARE
 PRESENTED IN TABULAR FORM, AND ARE COMPARED
 GRAPHICALLY WITH THE THEORETICAL APPROXIMATION TO
 THE RATE OF FALL OF SPHERES AND WITH THE ACCEPTED
 CURVE FOR SPHERES.
 KEYW TERMINAL VELOCITY, REYNOLDS NUMBERS, FALL
 VELOCITY, DRAG COEFFICIENTS
 CODE 7734F
- AUTH SATO T., SUZUKI, Y., KASHIMACI M., BANIC M., OKUI
 Y.
 TITLE A METHOD FOR REMOTE DETECTION OF OIL SPILLS USING
 LASER-EXCITED RAMAN BACKSCATTERING AND
 BACKSCATTERED FLUORESCENCE
 PUBL IEEE JOURNAL OF OCEANIC ENGINEERING, VOL. 13,
 NO. 1, JAN. 1978
 ABST A LASER METHOD FOR THE REMOTE DETECTION OF OIL
 PRESENT AS A POLLUTANT IN THE SEA WATER USING
 RAMAN BACKSCATTERING AND BACKSCATTERED
 FLUORESCENCE IS DISCUSSED.
 KEYW LASER METHOD, DETECTION, BACKSCATTERING,
 BACKSCATTERED FLUORESCENCE
 CODE 7657F
- AUTH SAUNDERS R.O., VAN LOON L.S.
 TITLE WATER RESOURCES RESEARCH PROGRAM, NEARSHORE
 CURRENTS AND WATER TEMPERATURES IN SOUTHWESTERN
 LAKE MICHIGAN
 PUBL BUREAU OF ENVIRONMENTAL SYSTEMS DIV., ARCONNE
 NATIONAL LABORATORY, MSL/MP 70-7, MAY 1976, JUNE -
 DEC. 1975
 ABST THE PRESENT STUDY WAS DESIGNED TO INVESTIGATE THE
 TEMPORAL AND SPATIAL COMPLEXITY OF CURRENTS OFF SO.
 CHICAGO, ILL., AND E. CHICAGO, IND.
 KEYW COASTAL CURRENTS, SPATIAL AND TEMPORAL VARIABILITY
 CODE 0520F
- AUTH SAUNDERS R.O., VAN LOON L.S.
 TITLE WATER TEMPERATURES IN SOUTHWESTERN LAKE MICHIGAN.
 PROGRESS REPORT, JUNE-DECEMBER, 1975
 PUBL ARCONNE NATIONAL LAB., ILL. MAY 1976
 CODE 05114F
- AUTH SAVER W.F., REYNOLDS V.
 TITLE OIL LAYER THICKNESS MEASUREMENT
 PUBL PAPER NO. 71-040, 16TH ANNUAL ISA CONF., 1971
 CODE 2070F
- AUTH SAWLEY
 TITLE ACOUSTICAL ENERGY DECAY IN PIPING SYSTEMS
 PUBL SERI PUBL.
 ABST A METHOD IS DESCRIBED FOR PREDICTING THE DECAY OF
 ACOUSTICAL ENERGY IN A PIPING SYSTEM WITH DISTANCE
 ON THE PIPE FROM THE SOURCE OF NOISE. THE
 APPLICATION OF THE METHOD TO PRACTICAL SITUATIONS
 IS DISCUSSED.
 CODE 2003A
- AUTH SAWYER D.C.
 TITLE OIL SPILL SPECIALISTS EMERGE AS "SPECIAL" ENGINEERS
 AND MANAGERS BUSINESS MAGAZINE, OCT. 1975
 ABST REPORT ON COASTAL SERVICES. THIS PAPER DISCUSSES
 THE N.F. CLEANUP CONTRACTORS,
 KEYW CLEANUP, DISPERSANTS, CONTRACTORS
 CODE 2040F
- AUTH SCHAFERSTEIN C.F., LOAMY J.
 TITLE TESTING THE LOCKNEED DISC-DRUM OIL/WATER OIL
 RECOVERY SYSTEM
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1907,
 MAY 6-8, 1975
 ABST THIS PAPER DISCUSSES THE QUALIFICATION TESTING OF
 - THE LOCKNEED PROTOTYPES HIGH SEAS OIL RECOVERY
 SYSTEM.
 KEYW RECOVERY, INLAND POOL TEST, HIGH SEAS TESTS
 CODE 0954F
- AUTH SCHATTJURG P., HARRIS L.B., ADENA C.R., JACKSON
 B.P., KELLY C.M.
 TITLE OIL-WATER SEPARATION WITH NONCELLULOSE
 ULTRAFILTRATION SYSTEMS
 PUBL NAVAL SHIP RESEARCH AND DEVELOPMENT CENTER, FOR
 EPA 1975 CONFERENCE
 KEYW OIL-WATER SEPARATION, NONCELLULOSE
 ULTRAFILTRATION SYSTEMS
 CODE 0132F
- AUTH SCHWYIN J.E., GIBSON C.N., DEATON T.K.
 TITLE MEASUREMENTS OF TURBULENCE, TEMPERATURE AND
 SALINITY MICROSTRUCTURE IN THE UPPER LAYERS OF THE
 OCEAN-AN INTERCOMPARISON TEST
 PUBL SCRIPPS INSTITUTION OF OCEANOGRAPHY, UNIVERSITY OF
 CALIFORNIA, SAN DIEGO CA
 ABST SMALL SCALE FLUCTUATIONS OF TEMPERATURE,
 CONDUCTIVITY AND VELOCITY WERE MEASURED FROM TENDR
 BOOIES AT DEPTHS FROM 10-1000 METERS. RESULTS OF
 US TEMPERATURE MEASUREMENTS BELOW THE BASE OF A
 WIND MIXED LAYER ARE PRESENTED.
 KEYW TEMPERATURE INVERSION, FOSSIL TEMPERATURE
 TURBULENCE, SPECTRAL ANALYSIS
 CODE 7707 F
- AUTH SCHIFF E.J.
 TITLE AIR BUBBLE BREAKWATER
 PUBL HYDRODYNAMICS LABORATORIES
 ABST THE CONSIDERATION OF PROPERTIES OF BUBBLY WATER, THE
 DESIGNING OF BARRIERS INTO A SINGLE BUBBLE SCREEN,
 AND FINALLY THE TRANSMISSION THROUGH A SERIES OF
 EQUALLY SPACED SCREENS.
 CODE 0000F
- AUTH SCHIRRE G.R., GOODIER J.L.
 TITLE INFORMATION FOR FIGHTING OIL POLLUTION, A CASE
 HISTORY
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1973,
 APR. 1975
 ABST THIS PAPER OUTLINES A WINDY COASTAL POLLUTION
 CONTROL PROGRAM AND STRAIGHT AT A MULTI-USE TEST
 SITE IN MASS.
 KEYW PREVENTION, CONTROL, GOVERNMENT/INDUSTRIAL
 COOPERATION
 CODE 0631F
- AUTH SCHINDLER H.D., TRYPAL R.D.
 TITLE CONTINUOUS - PHASE MASS TRANSFER COEFFICIENTS FOR
 LIQUID EXTRACTION IN AGITATED VESSELS
 PUBL ATCHE JOURNAL, VOL. 14, NO. 9, SEPT. 1968
 ABST IN THIS WORK, INTERFACIAL AREA WAS DETERMINED IN
 SITU BY A LIGHT TRANSMISSION TECHNIQUE.
 KEYW CONTINUOUS PHASE, MASS TRANSFER, LIQUID
 EXTRACTION, LIGHT TRANSMISSION
 CODE 0070F
- AUTH SCHITZBERG P., JACKSON D.
 TITLE REMOTE SAMPLER FOR DETERMINING RESIDUAL OIL
 CONTENT OF SURFACE WATERS
 PUBL NAVAL SHIP RESEARCH AND DEVELOPMENT CENTER, 1973
 CONFERENCE
 KEYW REMOTE SAMPLER, DETERMINATION, CONTENT
 CODE 0501A
- AUTH SCHNEIDER L.
 TITLE A REVIEW OF OIL HANDLING PROBLEMS AT OFFSHORE
 TERMINALS - PART II PROGRAM FOR EXPERIMENTALLY
 EVALUATING ADVANCED OIL BARRIERS
 PUBL US NATIONAL MARITIME RESEARCH CENTER, REPORT NO.
 NMRC-272-23100-014
 CODE 0730A
- AUTH SCHMIDT D., FERO L.B.
 TITLE ODOM CORP. OIL SPILL
 PUBL EPA, SURVEILLANCE AND ANALYSIS DIV., BIOLOGICAL
 SERVICES BRANCH, 1975 CONFERENCE
 ABST PAPER INCLUDES SAMPLING METHODS OF MACRO
 INVERTEBRATE, FISH, PERIPLANKTON, SEDIMENT, WATER
 SAMPLES, AND HYDROCARBON ANALYSIS.
 KEYW SAMPLING METHODS, SEDIMENT, FISH
 CODE 01514F
- AUTH SCHWARTZBERG M.
 TITLE THE MOVEMENT OF OIL SPILLS
 PUBL PHYSIC-BIOLOGICAL EFFECTS
 ABST THE EFFECTS OF WINDS AND CURRENTS AND THE PHYSICAL
 PROPERTIES OF OIL AND WATER ON THE DRIFT RATES OF
 OIL SPILLS WERE STUDIED IN TESTS CARRIED OUT IN A
 COMBINED WIND BASH AND TUNNEL
 KEYW WINDS, WAVES, AND CURRENTS, DRIFT RATES
 CODE 0044F
- AUTH SCHWARTZBERG M.C.
 TITLE SPREADING AND MOVEMENT OF OIL SPILLS
 PUBL WATER POLLUTION CONTROL RESEARCH SOCIETY, OTIS.

- ABST PB197 052, MAR. 1970
THE SPREADING AND MOVEMENT OF OIL SPILLS ON WATER WERE INVESTIGATED. AREAS FOR SPILLS WHICH FORM LENSES WERE MEASURED AND CORRELATED.
KEYW OIL WATER INTERFACES, DRIFTING, WAVE/WIND
CODE 25617
- AUTH SCHWARTZBERG N.C., TRENKAL R.E.
TITL FLUID AND PARTICLE MOTION IN TURBULENT STIRRED TANKS
PUBL 1 AND 2C FUNDAMENTALS, VOL. 7, FEB. 1968
ABST DIFFERENT EQUATIONS DESCRIBING PARTICLE MOTION IN A TURBULENT FLUID WERE APPLIED TO A FLOW MODEL FOR TURBULENT STIRRED TANKS. THE CALCULATED SLIP VELOCITIES INDICATE THAT PARTICLE TO FLUID MASS TRANSFER CANNOT BE EXPLAINED IN TERMS OF A SIMPLE SLIP VELOCITY MODEL.
CODE 50754
- AUTH SCOTT J.C., MUSTER D.
TITL THE INFLUENCE OF SURFACE ACTIVE CONTAMINATION ON THE INTERACTION BETWEEN WIND AND WAVES
PUBL HOUSTON UNIV. HOUSTON TEXAS, AD 784159
CODE 20474
- AUTH SEARLE W.F.
TITL THE OIL SPILL CONTROL SYSTEMS TAILORED FOR SPECIFIC TASKS.
PUBL OCEAN INDUSTRY, VOL. 5, NO. 7, JULY 1970
ABST THIS ARTICLE REPORTS ON TWO SYSTEMS FOR CONTAINMENT AND REMOVAL: 1) THE OIL SCRUBBER FOR CALM WATER IN SHORE OIL SLICER REMOVAL AND 2) THE TSP BOOM FOR USE IN CONTAINING FLOATING OIL SLICERS IN ROUGH, OFFSHORE WATERS.
KEYW CONTAINMENT, REMOVAL, SCRUBBER, BOOM
CODE 30298
- AUTH SEMINER A.J.
TITL AN OCEANIC GENERAL CIRCULATION MODEL WITH BOTTOM TOPOGRAPHY
PUBL DEPT. OF METEOROLOGY, UNIV. OF CAL. DEC. 21, 1974
ABST DOCUMENTS A NEW OCEANIC GENERAL CIRCULATION MODEL, RECENTLY CONSTRUCTED AT UCLA. THE MODEL ALLOWS PREDICTION OF THE THREE DIMENSIONAL FIELDS OF VELOCITY, TEMPERATURE AND SALINITY IN AN OCEAN OF ARBITRARY GEOMETRY. THE COMPUTER PROGRAM FOR THE MODEL MINIMALIZES CORE STORAGE. A DISCUSSION OF THE PROGRAM AND A COMPLETE PROGRAM LISTING ARE ENCLOSED IN THE REPORT.
KEYW VELOCITY, TEMPERATURE, SALINITY, CORE STORAGE
CODE 70981
- AUTH SHAPIRO A., FRICKSON A.
TITL ON THE CHANGING SIZE SPECTRUM OF PARTICLE CLOUDS UNDERSTANDING EVAPORATION, COMBUSTION OR ACCELERATION, 1954
PUBL HEAT TRANSFER AND FLUID MECHANICS INST., JUNE 21-23, 1954
ABST A THEORETICAL TREATMENT IS GIVEN SHOWING HOW THE SIZE DISTRIBUTION OF A CLOUD OF PARTICLES CHANGES AS THE RESULT OF EVAPORATION, COMBUSTION, OR ACCELERATION. SOLUTIONS TO THE DIFFERENTIAL EQUATION ARE THEN OBTAINED FOR A NUMBER OF SPECIAL PROBLEMS OF INTEREST TO EVAPORATION AND COMBUSTION.
KEYW DISTRIBUTION OF CLOUD PARTICLES, EVAPORATION, COMBUSTION, ACCELERATION
CODE 71387
- AUTH SHELL OIL CO.
TITL EQUILIBRIUM
PUBL EQUILIBRIUM VOL. 9, NO. 3, FALL 1974
ABST VARIOUS ARTICLES PERTAINING TO SPILLS.
KEYW SPILLS, INDUSTRIAL APPROACH, MARINE ENVIRONMENT
CODE 6578F
- AUTH SHELTON R.
TITL DISPERSANT TOXICITY TEST PROCEDURE
PUBL UNITED KINGDOM MINISTRY OF AGRICULTURE FISHERIES AND FOOD, ENGLAND
ABST IN THIS REPORT THE INVESTIGATION OF THE TOXICITY OF CHEMICALS USED TO DISPERSER OIL AT SEA AND ON THE SHORE IS DISCUSSED IN RELATION TO THE GENERAL PROBLEMS OF THE EFFECTS ON FISHERIES AND MARINE LIFE AND THE METHODS USED TO DEAL WITH OIL SPILLS.
KEYW TOXICITY, DISPERSANTS, FISHERIES, MARINE LIFE
CODE 7144F
- AUTH SHELTON R.C.J.
TITL EFFECTS OF OIL AND OIL DISPERSANTS ON THE MARINE ENVIRONMENT
PUBL PROCEEDINGS OF THE ROYAL SOCIETY OF LONDON, 8, VOL. 177, 1972
CODE 50564
- AUTH SHONTING D.W.
TITL BHOUDI ISLAND SOUND SQUARE KILOMETER STUDY: 1967
PUBL JOURNAL OF GEOPHYSICAL RESEARCH, VOL. 74, NO. 13, JUNE 20, 1969
ABST THIS PAPER DISCUSSES THE PROBLEM OF THE PREDICTION OF THE TIME VARIABLE DISTRIBUTION OF OCEANOGRAPHIC PARAMETERS AT A GIVEN LOCATION OF THE OCEAN.
KEYW PATTERN, ENERGY DISTRIBUTION, SPACE AND TIME GRADIENTS
CODE 2872F
- AUTH SHONTING D.W., COHN G.S.
TITL ON THE SEASONAL DISTRIBUTION OF TEMPERATURE AND SALINITY IN BHOUDI ISLAND SOUND
PUBL REPORT FROM LIMNOLOGY AND OCEANOGRAPHY, VOL. 15, NO. 1, JAN. 1970
ABST THE TEMPERATURE AND SALINITY OF BHOUDI ISLAND SOUND WERE MEASURED BETWEEN JULY 1967 AND JULY 1968.
KEYW TEMPERATURE AND SALINITY, THERMOCLINE, SALINITY PATTERNS, THERMAL ENERGY
CODE 2871F
- AUTH SMITHMAN R.A., JACKSON P.L., FELDMAN E.A.
TITL PROBLEMS OF IMAGING OCEAN WAVES WITH SYNTHETIC APERTURE RADAR
PUBL ENVIRONMENTAL RESEARCH INSTITUTE OF MICHIGAN-AUGUST 1977
ABST PROGRESS IS REPORTED ON THREE TASKS DESIGNED TO PROVIDE INFO TO EVALUATE THE OPERATIONAL USE OF SAR. TASK 1: A LIMITED LITERATURE SEARCH. TASK 2: SOLUTIONS TO SAR SIGNAL PROCESSING PROBLEMS WERE DEVELOPED. ALSO A DIGITAL CORRECTION ALGORITHM WAS DEVELOPED AND TESTED. TASK 3: AN ANALYSIS OF OPTICAL TRANSDUCER OPERATIONS ON SAR WAVE TRACERY WAS PERFORMED.
KEYW OCEAN WAVES, RADAR SENSING, SAR IMAGERY, DIGITAL PROCESSING
CODE 7700 F
- AUTH SMOLARSKI R.V.
TITL MOLECULAR PHYSICS OF THE SEA PART B
PUBL TRANS. FROM FIZIKA MOLEK. MOSCOW, AD 711957
CODE 0405F
- AUTH SMULLIKOWITZ F., JEFFERY P.C.
TITL DISPERSANTS FOR OIL SPILL CLEAN-UP OPERATIONS: CHALLENGE AND CONTAINMENT AT SEA
PUBL WAPPA SPRING LABORATORY, LB 1051001, 1974
ABST THIS REPORT DESCRIBES THE CONSIDERABLE DIFFICULTIES EXPERIENCED WITH THE LOADING, UNLOADING AND USAGE OF STEEL DRUMS OF DISPERSANT CLEAN-UP, DISPERSANTS, STEEL DRUMS, TANK STORAGE.
KEYW CODE 7427F
- AUTH SICRA R.W.
TITL OIL RECOVERY PROGRAMS
PUBL PROJECT 15080 EMP AUG. 1977
ABST AIR MODULATED VACUUM-OIL FOAMS RECOVERY COLLECTION OF SPILLED OIL
CODE 6364P
- AUTH STEPHENS A.
TITL STATEMENT BY RADH. ABE STEPHENS
PUBL PRESENTED BEFORE THE HOUSE COMMITTEE ON SCIENCE AND TECHNOLOGY SUBCOMMITTEE OF ENERGY RESEARCH, DEVELOPMENT, AND DEMONSTRATION, JULY 8, 1977
ABST REMARKS ARE LIMITED TO COAST GUARD ACTIVITIES, WITH AN OVERVIEW OF GENERAL ACTIVITIES AND RESPONSIBILITIES.
KEYW VESSEL SAFETY, PORT SAFETY, POLLUTION INCIDENTS, AND CLEANUP
CODE 5093F
- AUTH STEPHANSON N., WOOD E.C.
TITL MARYLAND'S EXPERIENCE IN OIL SPILL PREVENTION AND CONTROL
PUBL STATE OF MARYLAND, WATER RESOURCES ADMIN., FOR EPA 1975 CONFERENCE
ABST AN EXISTING SPILL PREVENTION AND RESPONSE PROGRAM IS DESCRIBED UTILIZING THE STATE WRA. EMPHASIS IS ON PREVENTION.
KEYW PREVENTION, CONTROL, MARYLAND
CODE 0077F
- AUTH SIMPSON A.C.
TITL OIL EMULSIONS AND COMMERCIAL SHELLFISH FIELD STUDY.
CODE 90514
- AUTH SITTEG W.
TITL OIL SPILL PREVENTION AND REMOVAL HANDBOOK
PUBL POLLUTION TECHNOLOGY REVIEW NO. 11, ENERGY TECHNOLOGY REVIEW NO. 7, OCEAN TECHNOLOGY REVIEW NO. 11, WISNES DATA CORP., PARK RIDGE, N.J. 1974
ABST THIS BOOK ATTEMPTS TO ORGANIZE AND CLARIFY THE MANY WAYS AND MEANS NOW AVAILABLE IN THIS LITERATURE FOR THE REMOVAL OF THE CONTAMINATING OIL FROM BOTH THE OCEAN SURFACES AND ITS BEACHES.
KEYW CLEANUP, ENERGY SOURCE, WISNAPS
CODE 40188
- AUTH SIYADIEP H.O., MIKOLA P.L.
TITL MEASUREMENT OF EVAPORATION RATES FROM OIL SLICKS ON THE OPEN SEA
PUBL RATE OF OIL
ABST DISCUSSES DEVELOPMENT OF GAS CHROMATOGRAPHIC METHOD OF ANALYSIS TO MEASURE THE TIME DEPENDENT EXTENT OF EVAPORATION FROM AN OIL SLICK AT OPEN SEA.
KEYW SEEPS, EVAPORATION, SEA SURFACES
CODE 0854F
- AUTH SMALL S.
TITL WHAT'S BEST IN SUPER-TERMINALIST
PUBL MARINE ENGINEERING SOCIETY, INC.
ABST THIS PAPER ATTEMPTS TO GIVE SOME INSIGHT INTO THE PROBLEM OF ENGINEERING DEVELOPMENT FOR

- WITH ANALYTIC SOLUTIONS FOR AN INSTANTANEOUS POINT SOURCE HAVE SHOWN GOOD RESULTS IN RESOLVING THE WASTE MOTION. THIS MODEL WILL PROVIDE A USEFUL TECHNIQUE TO STUDY THE MOTION OF SEDIMENT, BREACHED SPOILS, AND OTHER PARTICULATE WASTE LOADS DEPOSITED IN COASTAL WATERS.
- CODE - 7754F
- AUTH SPAULDING R.L., BROWN C.A., WHITE P.R.
 TITLE APPLYING WATER QUALITY MODEL TO POLLUTION MANAGEMENT
 PUBL NOAA SEA Grant, WRI, MARINE TECHNICAL REPORT 26, 1974
 ABST TO HELP PROVIDE TECHNICAL ALTERNATIVES THE AUTHORS DEVELOPED A WATER QUALITY MODEL FOR THE DISSOLVED OXYGEN-BIOCHEMICAL OXYGEN DEMAND SCHEME FOR BARRAGANSETT BAY
 REYS WATER POLLUTION MANAGEMENT, DISPOSAL, SELF CLEANING CAPACITIES
 CODE 7641F
- AUTH SPILLANE L.T.
 TITLE MOVEMENT OF OIL ON THE SEA SURFACE
 PUBL AUSTRALIAN METEOROLOGICAL MAG., VOL. 10, NO. 4, 2072F
 CODE 7642F
- AUTH SPRIGG R.C., REEWIN S.
 TITLE POLLUTION AND CONSERVATION OF THE AUSTRALIAN COASTLINE
 PUBL AUSTRALIAN PETROLEUM EXPLORATION ASSOCIATION JOURNAL, 1971
 ABST DISCUSSION ON OIL POLLUTION WHILE DRILLING ON THE GREAT BARRIER REEF, ALSO INCLUDES MENTION OF ADVANTAGES OF OFFSHORE DRILLING.
 CODE 7643F
- AUTH STAINFEN D.W.
 TITLE EFFECTS OF UPTAKE AND DISCHARGE OF PETROLEUM HYDROCARBONS ON THE RESPIRATION OF THE SOFT-SHELL CLAM, MYA ARENARIA
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST A WINTER SPILL CONDITION WAS SIMULATED IN WHICH VOLUM. SOFT SHELL CLAMS WERE EXPOSED TO SUBACUTE CONCENTRATIONS OF NO. 2 FUEL OIL-IN-WATER EMULSIONS FOR 28 DAYS.
 REYS RESPIRATION, PETROLEUM EMULSION, PETROLEUM ACCUMULATION, DEGENERATION
 CODE 7644F
- AUTH STAINFEN D.W.
 TITLE PRELIMINARY OBSERVATIONS ON THE MORT OF ACCUMULATION OF NO. 2 FUEL OIL BY THE SOFT SHELL CLAM, MYA ARENARIA.
 PUBL NUTIGES UNIV., DEPT. OF ZOOLOGY AND PHYSIOLOGY FOR EPA CONFERENCE 1975
 REYS OBSERVATIONS, MODE OF ACCUMULATION, NO. 2 FUEL OIL, SOFT SHELL CLAM
 CODE 8135A
- AUTH STANULES A.
 TITLE FINAL REPORT - THE VORTER PRINCIPLE, A METHOD FOR CONCENTRATING MATERIALS FROM A LIQUID PHASE
 PUBL NAVAL RESEARCH LAB., AD 750007, NAL-60-2401
 CODE 8603A
- AUTH STANFORD A.F., JARVIS B.N.
 TITLE WAYS AND MEANS OF DEALING WITH OIL POLLUTION
 PUBL IN SYMPOSIUM ON MARINE POLLUTION LONDON ROYAL INSTITUTE OF NAVAL ARCHITECTS
 CODE 8101B
- AUTH STANLEY H.G., BAPLANER D.W.
 TITLE FINAL REPORT - A BIBLIOGRAPHY ON OCEAN WASTE DISPOSAL SECOND EDITION
 PUBL EPA, OCEAN DISPOSAL PROGRAM, PD 265 831, SEPT. 1976, REPORT NO. 666000-17
 ABST THIS RESEARCH BIBLIOGRAPHY WAS PREPARED FOR THE OFFICE OF WATER PROGRAM OPERATIONS, USFPA. IT IS RESTRICTED TO DOCUMENTS RELEVANT TO THE FIELD OF OCEAN WASTE DISPOSAL. IT IS PRIMARILY LIMITED TO RECENT PUBLICATIONS IN THE CATEGORIES OF: GENERAL OCEAN WASTE DISPOSAL, NON-POINT SOURCE, OCEANIC DISPOSAL OF RADIOACTIVE WASTES, AT-SEA INCINERATION.
 REYS OCEAN WASTE DISPOSAL, COASTAL ZONE MANAGEMENT, BRIDGE SPILL
 CODE 7211F
- AUTH STARS R.P., ROSS D.E., MORRISON R.
 TITLE OIL SPILL DECISIONS FOR DEBRIS DISPOSAL VOL. II
 PUBL EPA-600/2-77-153B, AUG. 1977
 ABST THIS REPORT WAS PREPARED TO GUIDE PERSONS RESPONSIBLE FOR DISPOSING OF OIL SPILL CLEANUP DEBRIS IN SELECTING SUITABLE SITES FOR DEBRIS DEPOSITION AND IN EFFECTING PROPER DISPOSAL OPERATIONS.
 REYS DEBRIS DISPOSAL, CLEANUP, BRIDGE PLANNING
 CODE 7641F
- AUTH STEGMAN J.J.
 TITLE INFLUENCE OF ENVIRONMENTAL CONTAMINATION ON CYTOTOXICITY OF 450 MIXED-SPECIES BRYOPHORES IN FISH: IMPLICATIONS FOR RECOVERY IN THE WILD MARSHES
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST DISCUSSION ON LEVELS OF CONTAMINANTS IN BRYOPHORE
- REYS OPTIMUM HYPERPLASTIC IN CONTAMINATED MARSHES.
 REYS MIXED SPECIES BRYOPHORES, ENVIRONMENTAL CONTAMINATION, RECOVERY
 CODE 7641F
- AUTH STEINHART C.E. AND J.S.
 TITLE OIL SPILL - A CASE STUDY OF THE SANTA BARBARA OIL SPILL
 PUBL OCEANARY PRESS, BELMONT, CALIFORNIA 1977
 ABST THIS BOOK EXAMINES IN MINUTE DETAIL ALL OF THE SANTA BARBARA'S POLITICAL, ECOLOGICAL, AND SCIENTIFIC IMPLICATIONS. IT ASSESSES THE ENVIRONMENTAL CONCERNS INVOLVED AS WELL AS THOSE OF THE PETROLEUM INDUSTRY AND THE GOVERNMENTAL AGENCIES.
 CODE 8060B
- AUTH STEINMAN G.C., CHAPPEL R.P.
 TITLE THE MARITIME ADMINISTRATION PROGRAM FOR THE PREVENTION AND CONTROL OF OIL POLLUTION FROM VESSELS
 PUBL ENVIRONMENTAL ACTIVITIES GROUP, MARITIME ADMIN., FOR EPA 1975 CONFERENCE
 ABST THIS PAPER PROVIDES AN OVERVIEW OF THE MARITIME ADMIN. PROGRAM TO ABATE AND CONTROL OIL POLLUTION FROM SHIPS. RECOMMENDATION FOR FUTURE ACTION TO ABATE SHIP-GENERATED POLLUTION AT THE NATIONAL AND INTERNATIONAL LEVELS ARE PROVIDED.
 REYS MARITIME ADMINISTRATION PROGRAM, ABATEMENT, FEDERAL, NATIONAL, INTERNATIONAL
 CODE 8060B
- AUTH STEWART J.E., MAPS E.J.
 TITLE DISTRIBUTIONS AND ABUNDANCE OF HYDROCARBON-UTILIZING BACTERIA IN SEDIMENTS OF CHTHARTIC BAY, NOVA SCOTIA, IN 1976
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1978
 ABST AN EXTENSIVE RE-CERMINATION OF CHERBUCTO BAY, NOVA SCOTIA, SEDIMENTS WERE CARRIED OUT IN THE SUMMER OF 1976 FOR COMPARISON WITH DATA OBTAINED EARLIER AFTER THE MAJOR OIL SPILL IN 1970.
 REYS HYDROCARBON, HYDROCARBON-UTILIZING BACTERIA, PETROLEUM SEDIMENT
 CODE 7645F
- AUTH STEWART J.R.
 TITLE JET OIL RECOVERY DEVICE
 PUBL APPLIED CONTROL TECHNOLOGY
 ABST THIS PAPER IS PURELY DESCRIPTIVE AND FINDINGS REFLECT ACTUAL PHYSICAL CONSTRUCTION AND TESTS ONLY.
 REYS RECOVERY, JET WATER SYSTEM, SURFACE TENSION
 CODE 8014F
- AUTH STEWART R.J.
 TITLE OIL SPILL TRAJECTORY STUDIES FOR ATLANTIC COAST AND GULF OF ALASKA
 PUBL US COUNCIL ON ENVIRONMENTAL QUALITY, R11 1974
 CODE 7073A
- AUTH STEWART R.J., DEVAINEY J.M., CHAISSON R.E., SMITH L.B., PAY J.M., TRAVERS W.P., LONEY P.P.
 TITLE OIL SPILLS AND OFFSHORE DRILLING
 PUBL SCIENCE, VOL. 196, JAN. 1977
 ABST THIS REPORT DISCUSSES AN ARTICLE BY WILLIAM P. TRAVERS AND PENEY E. LONEY, DRILLING, TANKERS, AND OIL SPILLS ON THE ATLANTIC OUTER CONTINENTAL SHELF REIG ACT, 1974 P.741
 REYS DRILLING, TANKERS, BLOWOUTS
 CODE 7641F
- AUTH STEWART W.S.
 TITLE MICROBIOLOGICAL AND NATURAL PRODUCT SYSTEMS FOR THE PROTECTION OF COASTAL SHORELINES FROM OIL SPILLS AND OIL CONTAMINATION
 PUBL ENVIRON RESEARCH AND ENGINEERING CO., FOR EPA 1975 CONFERENCE
 ABST INFORMATION IS PRESENTED CONCERNING THE EFFECTIVE USES OF CONTAMINATION LEVELS OF THE MATERIALS REQUIRED TO AFFORD PROTECTION OF ROCKS AGAINST OIL CONTAMINATION, THE METHOD OF APPLICATION, THE EFFECTS OF TEMPERATURE, THE DURATION OF PROTECTION OFFERED, AND THE OVERALL EFFICIENCY OF THE SYSTEMS.
 REYS PROTECTION, MICROBIOLOGICAL AND NATURAL PRODUCTS SYSTEMS, CONTAMINATION
 CODE 8170A
- AUTH STIRLING A.C.
 TITLE PREVENTION OF POLLUTION BY OIL AND HAZARDOUS MATERIALS IN MARINE OPERATIONS
 PUBL 1967 PROCEEDINGS
 ABST STATISTICAL ANALYSIS OF 1964 OIL SPILLS
 CODE 3195B
- AUTH STOPPFER R.L., JONES E.C.
 TITLE WORTHY CONCEPT FOR SEPARATING OIL FROM WATER
 PUBL USCG, REPORT NO 61042/1, JAN. 1973
 CODE 8450F
- AUTH STRAUCHER D.
 TITLE FACTORS CAUSING ENVIRONMENTAL CHANGES AFTER AN OIL SPILL
 PUBL JOURNAL OF PETRO. TECHNOLOGY
 CODE 1248F
- AUTH STAMMANN C.

- TITLE** WHAT HAS BEEN THE EFFECT OF THE SPILL ON THE ECOLOGY IN THE SANTA BARBARA CHANNEL
PUBL ENTROPY 1974, ONTO UNIVERSITY LIBRARY, 617FAS, ONTO, ONT. 9701
ABST THIS PAPER DISCUSSES SOME OF THE PROBLEMS THAT COMPLICATED DETERMINATION OF EFFECTS.
KEYW ENVIRONMENTAL FACTORS, SYMBIOTIC EFFECTS, SANTA BARBARA CHANNEL
CODE 25417
- AUTH** STRAUGHAN, D.
TITLE SANTA BARBARA: A REAL OR IMAGINED DISASTER? PRESENTED AT THE SECOND INTERNATIONAL MARINE TECHNOLOGY ASSESSMENT CONFERENCE, OCT. 1973
ABST THIS PAPER PROVIDES SOME BIOLOGICAL BACKGROUND ON THE SANTA BARBARA OIL SPILL IN 1969 AND DISCUSSES BIOLOGICAL STUDIES SUBSEQUENT TO THIS OIL SPILL.
KEYW SAMPLING, ANALYTICAL TECHNIQUES, BIOLOGICAL IMPACT
CODE 26409
- AUTH** STRZEJSKI F.J., DEHLING P.T.
TITLE CHEMICAL TREATMENT OF OIL SPILLS
PUBL PROCEEDINGS OF JOINT CONFERENCE ON PREVENTION AND CONTROL OF OIL SPILLS, APRIL, PMPCA/DEC. 1969
CODE 50329
- AUTH** SUCMAN, M.
TITLE AN EXPERIMENTAL INVESTIGATION OF OIL SPREADING ON WATER
PUBL M.S. THESIS, DEPT OF MECH. ENGR., MIT, 1970
CODE 20744
- AUTH** SULLIVAN R.C., RICKENSTEIN E., STRIEFELSCH D.
TITLE THE SPREADING OF LIQUIDS ON LIQUIDS
PUBL JOURNAL OF COLLOID AND INTERFACE SCIENCE, VOL. 33, NO. 4, AUG. 1970
ABST STUDY OF SPREADING OF A HIGH SURFACE TENSION LIQUID AT THE FREE SURFACE OF A LOWER SURFACE TENSION LIQ. EFFECTS OF SURFACE TENSION AND CONCENTRATION DIFFERENCES AS WELL AS THAT OF VISCOSITY ARE EXAMINED.
KEYW SURFACE TENSION, CONCENTRATION DIFFERENCES, VISCOSITY
CODE 63075
- AUTH** SWISS, R.J.
TITLE PRESENCE OF POLYCYCLIC AROMATIC HYDROCARBONS IN COASTAL WATERS AND THE POSSIBLE HEALTH CONSEQUENCES
PUBL U.S. REGIONAL OFFICE FOR EUROPE, CITATION NO. 71-976-0247
CODE 11099
- AUTH** SULLIVAN C.E.
TITLE A COMPARATIVE STUDY OF THE EFFECTS OF EMULSIFIERS ON 1002 AND 99 1100 ON THREE AND SAND SPECIES
PUBL REP. OIL POLLUT. RES. UNIT, FLD. STUD. EDU., 1971, 10-21
CODE 10218
- AUTH** SURVEYOR AMERICAN BUREAU OF SHIPPING
TITLE WHEELS ACROSS THE SEA, MISSISSIPPI'S FUTURE SHIPBUILDING, PROFILE FORWARD, S.C. FROTA, DEWATER PORTS OFF USA, NAVAL CAREER TO 1/8TH SCALE, THE JEANETTE, NEWS BRIEFS
PUBL UNKNOWN
CODE REF.
- AUTH** SUTTON C., CALOFF J.A.
TITLE SOLUBILITY OF HIGH MOLECULAR WEIGHT N-PARAFFINS IN DISTILLED WATER AND SEAWATER
PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY
CODE 83609
- AUTH** SWADER F.A.
TITLE PERSISTENCE AND EFFECTS OF LIGHT OIL IN SOIL
PUBL CORNELL UNIV. EPA 1975 CONFERENCE
KEYW EFFECTS, LIGHT OIL, PERSISTENCE
CODE 81524
- AUTH** SWANSON J.C., SPAULDING W.L.
TITLE NUMERICAL SIMULATION OF OIL SPREADING ON AN ICE SURFACE
PUBL DEPT. OF OCEAN ENGINEERING, MIT
ABST USING AN EXPLICIT NUMERICAL TECHNIQUE, THE TWO DIMENSIONAL (P-Z) MOMENTUM EQUATIONS FOR OIL SPREADING ON AN OIL SURFACE ARE SOLVED.
KEYW OIL SPREAD ON ICE SURFACE, NUMERICAL TECHNIQUE, ICE PREDICTIONS
CODE 20434
- AUTH** SWEDHAR R., GRAMM A., ROLLBERG S.
TITLE EFFECTS OF OIL DISPERSANTS AND OIL EMULSIONS ON MARINE ANIMALS
PUBL WATER RESEARCH, VOL. 7, 1973
ABST ECOLOGICAL CONSEQUENCES OF DISPERSANTS AND OIL POLLUTION IN THE MARINE ENVIRONMENT ARE DISCUSSED.
KEYW DISPERSANTS, CLEANUP, TOXICITY
CODE 71269
- AUTH** SWEDHAR R.
TITLE TOXICITY TESTING AT EASTIMBERG ZOOLOGICAL STATION
PUBL ECOLOGICAL ASPECTS OF TOXICITY TESTING OF OIL AND DISPERSANTS, BYRON, L.B. EDITED, (PROG. OF A NORW. SHIP) PP 41-91, BARNING, ESSEA, APPLIED SCIENCES
- PUBLISHERS** 1974
CODE 10707
- AUTH** SWEDHAR R., GRAMM A.
TITLE BIOLOGICAL EFFECTS OF SURFACE ACTIVE AGENTS ON MARINE ANIMALS
PUBL MAR. BIOL. 9:189-201, 1971
CODE 88104
- AUTH** SWEDHAR R., GRAMM A., ROLLBERG S.
TITLE EFFECTS OF OIL DISPERSANTS AND OIL EMULSIONS ON MARINE ANIMALS
PUBL MAR. RES. 7:1049-1072, 1973
CODE 10469
- AUTH** SWIFT W.F.
TITLE MARINE ACUSTICAL HYDROCARBON DETECTION
PUBL SEVENTH ANNUAL CONFERENCE, APRIL 29 - MAY 2, 1973, PAPER NO. OTC 1803
CODE 04829
- AUTH** SWIFT W.
TITLE TAP BALLS IN THE SEA: A NEW SOURCE CONCEPT
PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2002, MAY 8-8, 1974
ABST THE CONTENTION OF THIS PAPER IS THAT NATURAL SEEPAGE COULD ACTUALLY ACCOUNT FOR A MAJOR PORTION OF THE TAP BALLS FOUND IN THE SEA.
KEYW TAPBALLS, SEEPAGE, NEW CONCEPT
CODE 08401
- AUTH** SWIFT W., TOMHILL C.J., HANEY B.A., BARATONI R.F., PETERSON P.L., DES VOIGES D.S.
TITLE REVIEW OF THE SANTA BARBARA CHANNEL OIL POLLUTION INCIDENT
PUBL FEDERAL WATER POLLUTION CONTROL ADMINISTRATION, WC, 14-17-330 PAPER NO. 150001A, JAN. 1969
ABST EFFECTS AND OPERATIONS CONCERNED WITH SANTA BARBARA OIL EMISSION INCIDENT.
KEYW SOURCES, EFFECTS, CONTROL, TREATMENT, TOXICITY
CODE 80427
- AUTH** SWIFT W.M., TOMHILL C.J., PETERSON P.L.
TITLE OIL SPILLAGE CONTROL
PUBL WATER 1969 CHEMICAL ENGINEERING PROGRESS SYMPOSIUM SERIES 87, VOL. 65, PUBL. BY AMERICAN INST. OF CHEMICAL ENGINEERS.
CODE 50158
- AUTH** SWIFT W.M., TOMHILL C.J., TEMPLTON W.L., BOSFRAN B.P.
TITLE OIL SPILLAGE PREVENTION CONTROL AND RESTORATION - STATE-OF-THE-ART AND RESEARCH NEEDS.
PUBL OIL POLLUTION: PROBLEMS AND POLICIES, BUREAU OF NATIONAL AFFAIRS, INC., 1969
CODE 50104
- AUTH** SWISHER R.D.
TITLE SURFACTANTS: FROM RECALCITRANT TO DOCILE
PUBL UNKNOWN
ABST FACTORS PROMPTING THE REDESIGN OF COMMERCIAL SURFACTANTS IN THE 1960'S, RELATIONSHIP OF THEIR CHEMICAL STRUCTURE TO THEIR BIOCOMPATIBILITY AND THEIR RESEARCH PATHWAYS INVOLVED IN REDESIGN.
KEYW COMMERCIAL SURFACTANTS, BIODEGRADATION, METABOLIC PATHWAYS
CODE 29471
- AUTH** TALTS A., BAYER J., MARTIN C., BREWIS D.
TITLE DISCOVERY, CONTAINMENT AND RECOVERY OF A JET FUEL STORAGE TANK LEAK: A CASE HISTORY
PUBL UNKNOWN
ABST THIS PAPER DISCUSSES SPILL PLANS FOR TERMINALS IN AREAS WITH HIGH SOIL SHOULD INCLUDE PROVISIONS FOR CONTAINMENT AND RECOVERY OF POTENTIAL LEAKS AND SPILLS FROM WITHIN THE GROUND.
KEYW CONTAINMENT, RECOVERY, TERMINALS
CODE 80577
- AUTH** TAYLOR G.
TITLE COMMENTS ON STANDARD METHODS FOR THE DETERMINATION OF THE RELATIVE TOXICITY AND VARIOUS OILS TO AQUATIC ORGANISMS
PUBL AMERICAN PETROLEUM INSTITUTE, PROCEEDINGS OF THE INDUSTRY-GOVERNMENT SEMINAR ON THE OIL SPILL TREATING AGENTS, WASHINGTON, D.C., PP. 80-85
KEYW TOXICITY, DISPERSANTS, AQUATIC ORGANISMS
CODE 10259
- AUTH** TAYLOR G.
TITLE STANDARD METHODS FOR DETERMINATION OF RELATIVE TOXICITY OF OIL DISPERSANTS AND MIXTURES OF DISPERSANTS AND VARIOUS OILS TO AQUATIC ORGANISMS
PUBL PMPCA NATIONAL MARINE WATER QUALITY LAB., CITATION NO. 970-04374
CODE 11274
- AUTH** TAYLOR W.B., WANG H.
TITLE MONTE CARLO SIMULATION OF OIL SLICK MOVEMENTS
PUBL A.S.C.E., WATERWAYS, HARBORS, AND COASTAL ENGINEERING DIVISION JOURNAL
CODE 04189
- AUTH** TAYLOR G.
TITLE THE ACTION OF A SURFACE CURRENT USED AS A DISPERSANT

PUBL RECEIVED 24 MARCH 1965
 ABST THE CONDITIONS UNDER WHICH AN OUTFLOW-PLACING SURFACE CURRENT CAN PREVENT PASSAGE OF WAVES COMING IN FROM THE SEA ARE INVESTIGATED MATHEMATICALLY.
 REVD OUTFLOW-PLACING SURFACE CURRENT, WAVES
 CODE 20210

AUTH TAYLOR H.E.J.
 TITLE TOMREY CANYON EXERCISE HOP UP
 PUBL ADMIRALTY CIL LABORATORY, REPORT NO 57, MARCH 1967
 ABST THE EFFECTING OF THE TOMREY CANYON ON THE 10TH OF MARCH 1967 CAUSED SEVERE OIL POLLUTION OF THE COASTLINE OF CORNWALL AND THE BRITISH COAST OF FRANCE. THIS PAPER DISCUSSES THE VARIOUS METHODS THE BRITISH AND FRENCH USED IN CLEAN-UP, THE EFFECT OF WIND AND WEATHER ON SUCH OPERATIONS AND VARIOUS TESTS ON COMMERCIAL MATERIALS.
 REVD TOMREY CANYON, CLEANUP, WIND AND WEATHER
 CODE 20100

AUTH TAYLOR H.E.J., WYLIE D.
 TITLE ADMIRALTY CIL LABORATORY, A.O.L. TECHNICAL NOTE NO. 51, AUG. 1967
 ABST THIS REPORT CONCERNS THE FRENCH APPROACH TO THE SPILLAGE FROM THE TOMREY CANYON ON MARCH 10, 1967. SINCE THE FRENCH WERE UNABLE TO USE DIVERGENTS BECAUSE OF THEIR VALUABLE TROPHEE FISHERIES THEY RELIED ON MECHANICAL MEANS AND SANDSTRA AND STRAW. IT DISCUSSES THE EFFECT ON THE BEACHES AND INCLUDES SEVERAL MAPS OF THE AFFECTED AREAS.
 CODE 20000

AUTH TEAL J.W., BURNS E., FARRINGTON J.
 TITLE ANALYSIS OF AROMATIC HYDROCARBONS IN INTERTIDAL SEDIMENTS RESULTING FROM TWO SPILLS ON NO. 2 FUEL OIL IN BUZZARDS BAY, MASS.
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1970
 ABST ANALYSIS OF THE AND THREE KING DOMESTIC HYDROCARBONS FROM THE WILD HARBOUR OIL SPILL IN SEPTEMBER 1969 AND THE WISNAP COVE OIL SPILL IN OCT. 1970, IN INTERTIDAL SAND SPHERULES, USING GLASS CAPILLARY GAS-CHROMATOGRAPHIC AND MASS-FRAGMENTOGRAPHIC ANALYSES.
 REVD AROMATIC HYDROCARBONS, GAS CHROMATOGRAPHY, MASS SPECTROMETRY
 CODE 20400

AUTH TELSON D.M.
 TITLE THE MOVEMENT OF OIL SLICKS AT SEA: PRELIMINARY MODEL STUDIES OF WIND AND CURRENT EFFECTS IN STUDY OF OIL SLICK DRIFT
 PUBL U.S.P. THESIS, 1969
 ABST THE PURPOSE OF THIS INVESTIGATION WAS TO CONTRIBUTE TO THE KNOWLEDGE OF THE BEHAVIOR OF OIL SPILLED ONTO THE SEA. ATTENTION IS FOCUSED ON THE DRIFT OF OIL SLICKS.
 REVD DRIFTING BEHAVIOR, DRIFT PROCESS, WIND AND CURRENT
 CODE 00530

AUTH TEMPLETON S.L.
 TITLE ECOLOGICAL EFFECTS OF OIL POLLUTION
 PUBL WATER POLLUTION CONTROL FEDERAL JOURNAL, VOL. 64, NO. 4, JUNE 1977
 ABST THIS PAPER DISCUSSES MONITORING OCEANS FOR POLLUTION AND POLLUTION PROTECTION, DISPENSANTS, ECOLOGICAL EFFECTS
 REVD POLLUTION, DISPENSANTS, ECOLOGICAL EFFECTS
 CODE 21100

AUTH TEMPLETON S.L., SUTTON E.A., DEAN S.W., ARNETT R.C., WELDON R.F., PLAYFELDER, MOORE R.J.
 TITLE OIL POLLUTION STUDIES IN LAKE MARACAIBO, VENEZUELA
 PUBL BATTLETT MEMORIAL INSTITUTE, PACIFIC NORTHWEST LAB., CREOLE PETROLEUM CORP. FOR EPA 1975 CONFERENCE
 ABST THE RESULTS IN A TWO-YEAR STUDY ON THE IMPACT OF OIL DISCHARGES ON THE FISHERY RESOURCES OF LAKE MARACAIBO, VENEZUELA ARE PRESENTED.
 REVD OIL DISCHARGES, FISHERY RESOURCES, EFFECTS, LAKE MARACAIBO, VENEZUELA
 CODE 01100

AUTH TEMPLETON S.L., WALSH P.C., BLACKMAN J.
 TITLE CHEMICAL DISPENSANTS FOR OIL SPILLAGE CLEANUP
 PUBL INDUSTRY GOVERNMENT SEMINAR, API, US DEPT. OF THE INTERIOR, 1970
 ABST DISCUSSION OF CHEMICAL DISPENSANTS AS TREATMENT AGENTS FOR OIL SPILL CLEANUP.
 REVD DISPENSANTS, TREATING AGENTS, EFFECTIVENESS, TOXICITIES
 CODE 50700

AUTH TEXAS A AND M UNIVERSITY
 TITLE ENVIRONMENTAL ASPECTS OF A SUPERTANKER PORT ON THE TEXAS GULF COAST
 PUBL TEXAS A AND M UNIVERSITY, SEA GRANT PROGRAM, DEC. 1972
 ABST THE OBJECTIVE OF THIS STUDY WAS TO CONDUCT AN EVALUATION OF THE ENVIRONMENTAL IMPACT OF A DEEP SEA PORT OFF THE TEXAS COAST.
 REVD ENVIRONMENTAL IMPACT, CONSTRUCTION AND OPERATION, PHYSICAL, BIOLOGICAL, AND CULTURAL FEATURES IMPACTED
 CODE 00020

AUTH TEZURA T., ARAMAKI K.
 TITLE TESTING OF NEW DEVICE FOR REMOVAL OF OIL SLICKS FROM THE SURFACE OF OPEN WATER
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 2000, MAY 2-8, 1976
 ABST MODEL BUILT OF A PROTOTYPE OF AN OIL RECOVERY BOAT TO CONDUCT WATER TANK TESTS. ACTUAL PERFORMANCE TESTS WERE CONDUCTED ON SEA WATERS.
 REVD RECOVERY, CATERMANS, TESTING
 CODE 05510

AUTH THOMAS J.P., PAULS C.F.
 TITLE SURVEY OF WASTEWATER DISCHARGE: ELMBROD O.F.B.
 PUBL REPORT NO. ENR-70-4
 CODE 04700

AUTH THOMAS W.L.M.
 TITLE COMPARISON OF OILED AND UNOILED INTERTIDAL COMMUNITIES IN CHEBARDICHO BAY, NOVA SCOTIA
 PUBL JOURNAL OF THE FISHERIES, VOL. 35, NO. 5, MAY 1970
 ABST THIS STUDY SHOWS SEVERAL ADDITIONAL BIOTIC EFFECTS OF OIL IN CHEBARDICHO BAY AND COMPARES PREVIOUS OILS.
 REVD HYDROCARBON, INTERTIDAL COMMUNITY, SEDIMENT
 CODE 20400

AUTH THOMAS W.L.M.
 TITLE EFFECTS OF BUNKER C OIL IN INTERTIDAL AND LAGOONAL BAYS IN CHEBARDICHO BAY, NOVA SCOTIA
 PUBL JOURNAL OF THE FISHERIES RESEARCH BOARD CANADA 30(11):83-90
 CODE 10040

AUTH THOMAS P.
 TITLE DEVELOPMENT OF A NEW DETECTOR FOR OIL IN WATER
 PUBL NAVAL AIR PROPULSION TEST CENTER, AD-603667, FEB. 1975
 ABST RECENT DECISIONS TO ENFORCE FEDERAL WATER POLLUTION CONTROL LAWS HAVE LED TO AN URGENT NEED FOR SENSITIVE RAPID AND SIMPLE FIELD METHOD FOR DETERMINATION OF OIL IN WATER. A NEW DETECTOR MEETING THESE REQUIREMENTS AND DESIGNED FOR SHIPBOARD USE WAS DESIGNED. THIS PAPER EXPLAINS THIS PROCEDURE.
 REVD CONTAMINATION, CONTAMINATION DETECTORS, BILGE CONTAMINATION
 CODE 63200

AUTH THORNTON S.W.
 TITLE TRAINING A CLEANUP RESPONSE TEAM
 PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
 ABST THIS PAPER DISCUSSES THE TRAINING OF A CLEANUP RESPONSE TEAM.
 REVD CLEANUP TEAMS, RESPONSE TEAM, JOB DESCRIPTION, OBJECTIVES, SEMINARS, PRACTICE
 CODE 00160

AUTH THORNTON S.W., DEFFABLE D.
 TITLE A NUMERICAL STUDY OF POLLUTANT DISTRIBUTIONS IN SEA WATERS CIRCULATIONS
 PUBL NATIONAL BUREAU OF STANDARDS, NBS-21400, TAD-18-2
 ABST IN THIS PAPER PRELIMINARY RESULTS OF A NUMERICAL STUDY OF THE EFFECT OF SEA WATERS CIRCULATIONS ON OIL POLLUTANT DISTRIBUTIONS ARE PRESENTED.
 REVD SEA WATERS CIRCULATIONS, CONTAMINATION, RECIRCULATION OF POLLUTANTS
 CODE 17000

AUTH THORNTON S.W., DIETHELM D.L.
 TITLE A NUMERICAL OIL TRAJECTORY FORECAST MODEL USED TO ASSESS THE HAZARD TO LONG ISLAND BEACHES FROM OIL ENTERING THE NEW YORK BIGHT AREA FROM FEB. 11-24, 1977
 PUBL RESEARCH SPONSORED BY NYNEX/SEA NEW YORK BIGHT PROJECT AND UNDER CONTRACT NO. F7-70-C-02-0016 WITH THE US ENERGY RESEARCH AND DEVELOPMENT ADMINISTRATION
 ABST THIS PAPER IS A REPORT ON OIL SPILLING INTO THE HUDSON RIVER FROM A GROUNDING PARTY ENTERING THE N.Y. BIGHT AREA ON FEB. 11, 1977.
 CODE 20770

AUTH TOLZENBACH S.D., MADSEN O.S., ADAMS E.E., POLLACK A.W., COOPER C.L.
 TITLE A REVIEW AND EVALUATION OF BASIC TECHNIQUES FOR THE REMEDIATION OF SURFACE OIL SLICKS
 PUBL API REPORT NO. WITSG 77-8, MARCH 1977
 ABST THE MOTIVATION FOR THE STUDY PRESENTED IN THIS REPORT IS THE NEED FOR A DETAILED REVIEW OF THE BASIC ANALYTICAL TECHNIQUES AVAILABLE FOR MAKING SUCH PREDICTIVE ESTIMATES.
 REVD LOCATION, SIZE, PROPERTIES, TRANSPORT, PHYSICAL, BIOLOGICAL AND CHEMICAL TRANSFORMATIONS
 CODE 61350

AUTH TONS
 TITLE OIL POLLUTION OF THE AND MATRES IN ENGLAND AND WALES
 PUBL WESSER WATER AUTHORITY
 ABST DESCRIBES THE SET UP OF TEN WATER AUTHORITIES IN ENGLAND TO MANAGE THE CLEANLINESS OF WATER AND TREATMENT OF SEWAGE. ALSO THE NEW CONTROL OF POLLUTION ACT 1974 IS EXAMINED.
 REVD WATER AUTHORITIES, CLEANLINESS AND SEWAGE

TREATMENT, CONTROL OF POLLUTION ACT 1974
CODE 0072F

AUTH TRACY M., WOLKES C.E., LEE R.G., SANDORN C.
TITLE RELATIVE TOXICITY AND DISPERSANT EVALUATIONS OF
OIL DISPERSING PRODUCTS

PUBL WATER-POLLUTION CONTROL FEDERAL JOURNAL, VOL. 41,
JULY-DEC. 1969

ABST THIS PAPER DISCUSSES RESULTS FROM TESTS ON OIL
DISPERSING PRODUCTS.

KEYW DISPERSANTS, TOXICITY, EMULSIFYING-EFFICIENCY
TESTS

CODE 2110F

AUTH TRAVERS W.B., LUMBY P.R.
TITLE DRILLING, TANKERS, AND OIL SPILLS ON THE ATLANTIC
OUTER CONTINENTAL SHELF

PUBL SCIENCE, VOL. 194, NO. 4267, NOV. 19, 1970

ABST THIS ARTICLE DISCUSSES FIRST THE GEOLOGIC
CONDITIONS WHICH HAVE CONTRIBUTED TO SPILLS ON THE
WEST COAST AND GULF COAST AREAS AND THEN DISCUSSES
THOSE WHICH WILL AFFECT DRILLING ON THE ATLANTIC
OUTER CONTINENTAL SHELF.

KEYW PREDICTING, TANKERS, DRILLING

CODE 2635F

AUTH TRAILER R.W.
TITLE MICROBIAL DEGRADATION OF PETROLEUM AT LOW
TEMPERATURE

PUBL MARINE POLLUTION BULLETIN, AUG. 1973, VOL. 4, 600-
81

ABST BACTERIA WERE ISOLATED FROM LITTORAL SEDIMENTS
COLLECTED IN MEMPHIS BAY, NOVA SCOTIA, AND FROM
OIL-CONTAMINATED SOIL ADJACENT TO A NATURAL OIL
SEEP AT CAPE SIMPSON, ALASKA. DATA ARE PRESENTED
ON THE RANGE OF HYDROCARBON UTILIZATION AND GROWTH
TEMPERATURE OF 2 BACTERIA, WHICH SUGGESTS THAT
BACTERIA EXISTING IN THESE ENVIRONMENTS PLAY A
SIGNIFICANT ROLE IN THE BIODEGRADATION OF
POLLUTANT HYDROCARBONS.

CODE 6173R

AUTH TRAILER R.W.
TITLE PETROLEUM DEGRADATION IN LOW TEMPERATURE MARINE
AND ESTUARINE ENVIRONMENTS

PUBL US DEPT. OF PLANT PATHOLOGY-ENTOMOLOGY, ANNUAL
REPORT NO. 1, OFFICE OF NAVAL RESEARCH CONTRACT
NO. N00014-69-0215-0015, TASK NO. NR 304-074,
MAY 1974

ABST STUDIES OF THE ENRICHMENT OF HYDROCARBONS AND FUEL
OIL UTILIZING BACTERIA FOLLOWING A SPILL IN
RHODE-ISLAND BAY.

KEYW BIODEGRADATION, BACTERIA, HYDROCARBONS

CODE 2931AF

AUTH TRAILER R.W., BHATTACHARYA I.S.
TITLE EFFECT OF A CHEMICAL DISPERSANT ON MICROBIAL
UTILIZATION OF PETROLEUM HYDROCARBONS

PUBL US DEPT. OF PLANT PATHOLOGY-ENTOMOLOGY, ANNUAL
REPORT NO. 1, OFFICE OF NAVAL RESEARCH CONTRACT
NO. N00014-69-0215-0015, TASK NO. NR 304-074,
MAY 1974

ABST STUDIES OF THE ENRICHMENT OF HYDROCARBONS AND FUEL
OIL UTILIZING BACTERIA FOLLOWING A SPILL IN
RHODE-ISLAND BAY.

KEYW BIODEGRADATION, BACTERIA, HYDROCARBONS

CODE 2931AF

AUTH TRAILER R.W., LUNDALL G.W.
TITLE PETROLEUM DEGRADATION IN LOW TEMPERATURE MARINE
AND ESTUARINE ENVIRONMENTS

PUBL US DEPT. OF PLANT PATHOLOGY-ENTOMOLOGY, OFFICE OF
NAVAL RESEARCH CONTRACT NO. N00014-69-0215-0015,
TASK NO. NR 304-074, ANNUAL REPORT NO. 2, MARCH
1975

ABST STUDIES OF THE ENRICHMENT OF HYDROCARBONS AND FUEL
OIL UTILIZING BACTERIA FOLLOWING A SPILL IN
RHODE-ISLAND BAY.

KEYW BIODEGRADATION, BACTERIA, HYDROCARBONS

CODE 2931AF

AUTH TRAINS W., KLEIN J., BERNHARDT J.
TITLE A METHOD FOR CALCULATING THE RATE OF EVAPORATION
AND THE CHANGE IN THE OROF SIZE DISTRIBUTION FOR
PURE SPHERES SUBJECT TO UNSTABILIZED AIR

PUBL PROJECT NO. 4092-C, CONTRACT NO. AF 33(600)-51.1.3,
NO. 407 04-1, MAY 1952

ABST LIMITATIONS AND EXTENSIONS OF THE ANALYSIS ARE
DISCUSSED.

KEYW EVAPORATION, MET-BUBBLE DEPRESSION, OROF-SIZE
SPECTRA

CODE 0053F

AUTH TRINDLE L.
TITLE OIL RECOVERY SYSTEMS, MARINE GOVERNMENT OIL SPILL
RECOVERY

PUBL LOCKHEED MISSILES AND SPACE CO. FOR USCG, SSIE NO.
67-2473

CODE 0451R

AUTH TROY G., MOLLINGER J.
TITLE THE MEASUREMENT OF OIL SPILL VOLUME BY A PASSIVE
MICROARRAY TRACER

PUBL NAVAL RESEARCH LAB., DEPT. OF TRANSPORTATION,
REPORT NO. 2415, MAY 1971, DOT USCG 2-21001

ABST THE DEVELOPMENT OF THE TRACER AND THE PROGRESS IN

ANALYSIS OF THE TRACER DATA REPRESENT A LARGE STEP
TOWARD AN AUTOMATIC SYSTEM FOR MAKING REAL-TIME
DETERMINATION OF OIL SPILL VOLUME.

KEYW THICKNESS, VOLUME, SPREADING, DETECTION, AIRBORNE
SYSTEM, REAL-TIME DETERMINATION

CODE 7620F

AUTH TURN W.
TITLE CONTACT OF OIL SPILLS - RECENT TECHNICAL
DEVELOPMENTS, POLLUTION CONTROL REPORT PART II

PUBL OCEAN INDUSTRY, JULY 1970

ABST THIS ARTICLE CONSIDERS SOME OF THE RECENT
DEVELOPMENTS IN CARRYING OUT STUDIES OF OIL SPILLS
AND MISCELLANEOUS AND DEALS WITH EQUIPMENT USED,
OIL SPILL STUDIES, EQUIPMENT, DEVELOPMENTS

KEYW

CODE 3026R

AUTH TULIN A.
TITLE UNSTEADY DENSITY CURRENT

PUBL HYDRODYNAMICS INC. OFFICE OF NAVAL RESEARCH
A THEORETICAL STUDY HAS BEEN UNDERTAKEN TO DEVELOP
BASIC RELATIONS ALONGING THEORETICAL CALCULATION
OF DENSITY CURRENT BEHAVIOR ASCERTAIN THE
RELEVANT PHYSICAL PHENOMENA AND THEIR RELATIVE
IMPORTANCE.

CODE 2510R

AUTH TULLY P.A.
TITLE REMOVAL OF FLOATING OIL SLICKS BY THE CONTROLLED
COMBUSTION TECHNIQUE

PUBL OIL ON THE SEA, PLENUM PRESS, 1969

ABST THIS ARTICLE DISCUSSES THE ADVANTAGES OF REMOVING
SLICKS BY BURNING AND VARIOUS TECHNIQUES FOR DOING
SO.

KEYW FLOATING OIL SLICKS, BURNING, TECHNIQUES

CODE 3034F

AUTH TURNSTALL F.
TITLE CONVINCED ON NEED FOR MORE OFFSHORE UNITS.

PUBL OCEAN INDUSTRY, VOL. 10, NO. 5, MAY 1973

ABST US PRESIDENT VISITS OFFSHORE DRILLING RIG

CODE 6120R

AUTH TURNER D.W.
TITLE OIL SPILL PREVENTION PRACTICES IN PIPELINES AND
TERMINALS

PUBL SOHIO PIPELINE CO. 1973 CONF.

CODE 6113R

AUTH TRAPP J.
TITLE SURFACE WATER MOVEMENTS IN NEW YORK HARBOR

PUBL LONG ISLAND UNIV., FOR USCG, SSIE NO. 62F-28

CODE 0455AF

AUTH UFA H., HART J.C.
TITLE FINE STRUCTURE TURBULENCE IN THE WALL REGION OF A
TURBULENT BOUNDARY LAYER

PUBL JOURNAL OF FLUID MECHANICS, VOL. 67, PART 1, 1973

ABST INFORMATION CONCERNING THE LARGE-SCALE
DISTURBANCE MECHANISM WHICH IS MAINLY RESPONSIBLE
FOR THE GENERATION OF TURBULENCE.

KEYW PLANE TURBULENT BOUNDARY LAYER, DISTURBANCE
MECHANISMS, TURBULENCE

CODE 6131F

AUTH UFF E.L.
TITLE LARGE CAPACITY PETROLEUM MEASUREMENT SYSTEMS
PRESENTED AT THE WINTER ASME ANNUAL MEETING,

HOUSTON, TEXAS, 30-DEC. 4, 1973

ABST SUPPLIERS LOADING AT RATES OF HALF A MILLION
BARRELS AN HOUR HAVE PRODUCED REQUIREMENTS OF
MEASURING PETRO. FLUIDS THAT ARE UNUSUAL.

KEYW TANKERS, LOADING RATES, MEASURING PETROLEUM FLUIDS

CODE 2901F

AUTH UHLM E.
TITLE FLUID MECHANICS OF MIXING

PUBL 4541

CODE 2957F

AUTH USA NATIONAL ACADEMY OF SCIENCES

TITLE ANNUAL VIEW OF OFFSHORE OIL AND GAS OPERATIONS

PUBL JOURNAL OF MARINE TECHNOLOGICAL SOCIETY, 0191,
1974

CODE 3066R

AUTH UYFOS S.T., EMMAN R.E., EDNOLLY A.C., JOHNSON
P.J.

TITLE CONCEPT DEVELOPMENT OF A POWERED ROTATING DISK OIL
RECOVERY SYSTEM

PUBL PHYSICAL RECOVERY
A SIMPLE TECHNIQUE FOR THE RECOVERY OF OIL FROM
THE WATER SURFACE IS THE USE OF ROTATING DISKS
WHICH ARE PRESENTIALLY WET BY THE OIL AND
COLLECTED FROM THE DISKS WITH WIPERS. THE
PRINCIPLE IS ALSO UTILIZED WITH ROTATING DEVICES.

KEYW RECOVERY, RECOVERY RATES, WAVES AND CURRENTS

CODE 0627F

AUTH WAGNER J.
TITLE OIL ON PUFFY SOUND, AN INTERDISCIPLINARY STUDY IN
SYSTEMS ENGINEERING

PUBL WASHINGTON SEA GRANT PUBLICATION, UNIV. OF
WASHINGTON PRESS, SEATTLE 1972

ABST OBJECTIVE: TO DEFINE OIL SPILL PROBLEM IN PUFFY
SOUND AND TO FORMULATE A MODEL FOR THE SOLUTION OF
THE PROBLEM.

- CODE 10650
 AUTH WALKER J.D., COLWELL R.A.
 TITLE SAMPLING DEVICE FOR MONITORING BIODEGRADATION OF OIL AND OTHER POLLUTANTS IN AQUATIC ENVIRONMENTS
 PUBL ENVIRONMENTAL SCIENCE AND TECHNOLOGY, VOL.11, NO. 1, JAN. 1977
 ABST A REPORT ON A SAMPLING DEVICE SUITABLE FOR MONITORING BIODEGRADATION UNDER FIELD CONDITIONS HAS BEEN DEVISED AND CONSTRUCTED. THE SAMPLER HAS BEEN SUCCESSFULLY EMPLOYED IN MONITORING BIODEGRADATION OF PETROLEUM IN SITU AT A MARSHLAND SITE IN THE CHESAPEAKE BAY.
 KEYW BIODEGRADATION, ENVIRONMENTAL IMPACT, AQUATIC ENVIRONMENTS
 CODE 2652H
- AUTH WALKER J.D., COLWELL R.A., MANNING M.L., FORD M.J.
 TITLE EXTRACTION OF PETROLEUM HYDROCARBONS FROM OIL CONTAMINATED SEDIMENTS
 PUBL J. ENVIRON. CONTAM. TOXICOL. 13
 CODE 5066P
- AUTH WALKER J.D., COLWELL R.A., PETRAKIS E.
 TITLE CHESAPEAKE BAY SEDIMENT BACTERIA AND THE BIODEGRADATION OF PETROLEUM
 PUBL REP. FROM - 1975 CONF. ON PREVENTION AND CONTROL OF OIL POLLUTION
 CODE 5017P
- AUTH WALKER J.D., COLWELL R.A., PETRAKIS E.
 TITLE PETROLEUM DEGRADATION BY BACTERIA FROM CHESAPEAKE BAY SEDIMENT: PART OF BACTERIAL HYDROCARBONS OF PETROLEUM SUBJECT TO DEGRADATION BY PRES. FACIES AND EMULSIFIC CULTURES
 PUBL J. GEN. MICROBIOL.
 CODE 5067P
- AUTH WALKER J.D., COLWELL R.A., PETRAKIS E.
 TITLE A STUDY OF THE BIODEGRADATION OF A SOUTH LOUISIANA CRUDE OIL, EMPLOYING COMPUTATIONAL MASS SPECTROMETRY
 PUBL UNIV. OF MARYLAND, MAR. RESEARCH AND DEVELOPMENT CO., FOR EPA THIS CONFERENCE
 KEYW BIODEGRADATION, SOUTH LOUISIANA CRUDE OIL, MASS SPECTROMETRY
 CODE 0154AP
- AUTH WALKER J.D., COLWELL R.A., PETRAKIS E.
 TITLE USE IN COMPUTATIONAL LOW-RESOLUTION MASS SPECTROMETRY TO ANALYZE BIODEGRADATION OF PETROLEUM
 PUBL CAN. J. MICROBIOL., 14:1
 CODE 5047P
- AUTH WALKER P.C.
 TITLE WATER POLLUTION BY OIL SPILLAGE
 PUBL JOURNAL WATER POLLUTION CONTROL FEDERATION, VOL. 43, NO. 6, JUNE 1971
 CODE 5018P
- AUTH WALKER P.C., BLACKMAN J.A., MENACEP C.H.
 TITLE OIL SPILL TREATING AGENTS A COMPENDIUM
 PUBL API, PROJECT NO. OS-6, CONTRACT NO. 21280003, 4042, MAY 1970
 ABST TO PROVIDE A SINGLE SOURCE ON AVAILABLE OIL SPILL TREATING AGENTS.
 KEYW TREATING AGENTS, WAREHOUSED MATERIALS, PRODUCTION RATES, READY REFERENCE
 CODE 4039B
- AUTH WALKER P.C., SMITH J.D., PETERSON P., POLENTI L.R.
 TITLE STUDY OF EQUIPMENT AND METHODS FOR REMOVING OIL FROM HARBOR WATERS
 PUBL UNKNDWN
 ABST THIS STUDY WAS PERFORMED TO IDENTIFY AND DESCRIBE THE MOST EFFECTIVE AVAILABLE SYSTEMS CONSISTING OF PRESENT OR NEW COMBINATIONS OF EXISTING EQUIPMENT, MATERIALS, AND TECHNIQUES.
 KEYW REMOVAL, MECHANICAL RECOVERY AND CONTAINMENT, CHEMICAL DISPERSANTS
 CODE 0517P
- AUTH WALLACE S.B.
 TITLE LEGAL ASPECTS OF THE 1975 MARINE POLLUTION CONVENTION: COMMENTS AND REFLECTIONS
 PUBL EPA, 1975 CONVENTION
 KEYW LEGAL ASPECTS, CONVENTION, COMMENTS
 CODE 0070P
- AUTH WANG H., CAMPBELL J.R., DITHERS J.D.
 TITLE COMPUTER MODELING OF OIL DRIFT AND SPREADING IN DELAWARE BAY
 PUBL OCS-88-1-78, OCEAN ENG. REP NO. 5, MARCH 1978, UNIV. OF DELAWARE, COLLEGE OF MARINE STUDIES
 ABST PROGRAM DESIGNED TO DELINEATE THE EFFECTS ON DELAWARE BAY OF CRUDE OIL TRANSFER AND UPSTREAM REFRESHMENT.
 CODE 8510A
- AUTH WANG H., YANG U.C., HUANG C.P.
 TITLE MODELING OF OIL EVAPORATION IN AN AQUEOUS ENVIRONMENT
 PUBL COLLEGE OF MARINE STUDIES, UNIV. OF DEL., OCS-88-1-78, NO. 5, DEC. 1978
 ABST RESEARCH ON THE EFFECTS OF CRUDE OIL TRANSFER AND UPSTREAM REFRESHMENT ON THE DELAWARE BAY. GOAL IS TO PROVIDE INFORMATION ON THE IMPACT OF OIL TRANSFER OPERATION IN DELAWARE BAY FOR DECISION MAKERS.
 KEYW NUMERICAL MODEL, CHARACTERISTICS OF OIL, WIND, TEMPERATURE, SIZE
 CODE 0515P
- AUTH WANG H.P.
 TITLE MODELING ON OFFSHORE POND
 PUBL WPI, MARINE TECHNICAL REPORT NO. 40, RECH. ENG. & APPLIED MECH., AGAA SEA GRANT, 1975
 ABST THE OBJECTIVES OF THIS REPORT ARE TO INVESTIGATE THE FEASIBILITY OF DIFFERENT NUMERICAL INTEGRATION SCHEMES AND TO DEVELOP A SUITABLE FINITE ELEMENT TO SIMULATE THE TIDAL CURRENTS IN BRIGHT POND.
 KEYW NUCLEAR POWER STATION, ENVIRONMENTAL RESEARCH, HYDRODYNAMICS
 CODE 2674I
- AUTH WANG S., WANG S.
 TITLE FINAL REPORT, A NUMERICAL MODEL FOR SIMULATION OF OIL SPREADING AND TRANSPORT AND ITS APPLICATION FOR PREDICTING OIL SLICK MOVEMENT IN BAY.
 PUBL USCG, REPT. OF TRANSPORTATION, TT-D-845-74-1, FEB. 1977
 ABST A COMPUTER MODEL FOR SIMULATING OIL SPREADING AND TRANSPORT HAS BEEN DEVELOPED. THE MODEL CAN BE UTILIZED AS A USEFUL TOOL IN PROVIDING ADVANCE INFORMATION AND THIS MAY GUIDE DECISIONS FOR AN EFFECTIVE RESPONSE IN CONTROL AND CLEANUP ONCE AN ACCIDENTAL SPILL OCCURS.
 KEYW NUMERICAL MODEL, OIL SPREAD AND TRANSPORT, PREDICTING MOVEMENT
 CODE 2674J
- AUTH WANG S., WANG S.
 TITLE A NUMERICAL MODEL FOR SIMULATION OF OIL SPREADING AND TRANSPORT
 PUBL NTIS REPORT NR-84078C 424
 ABST MICROFILME
 CODE 2674K
- AUTH WANG S., WANG S.
 TITLE MIXING OSCILLATION OF TWIN CYLINDERS IN A FREE SURFACE
 PUBL JOURNAL OF SHIP RESEARCH, MARCH 1971
 ABST THIS PAPER PRESENTS A SOLUTION OF THE TWO-DIMENSIONAL POTENTIAL PROBLEM ASSOCIATED WITH HARMONIC OSCILLATION OF A TWIN HULL BODY IN A FREE SURFACE.
 KEYW OIL RADIATION DYNAMICS, HYDRODYNAMICS, OSCILLATION
 CODE 0513I
- AUTH WARD R.P., DAVIES J.R.
 TITLE A COMPARISON OF THE RATES OF TRANSPORT OF OIL FROM SHIPWRECK SITES AND FROM OIL DISPENSER SITES IN THE WATER COLUMN TO THE BRITISH SOLENNETS
 PUBL INTERNATIONAL COUNCIL FOR THE EXPLORATION OF THE SEA, 1978, MARINE ENVIRONMENTAL QUALITY COMMITTEE, NO. CM 1978/15
 ABST OIL SLICKS WERE PUT ONTO THE SURFACE OF THE LARGE PLASTIC ENCLOSURES AND WERE TREATED WITH DISPERSANTS. THIS EXPERIMENT WAS CLEARLY SHOWN HOW THE FACTORS, MIXING AND DISPERSANT, CAN SIGNIFICANTLY AFFECT THE DECAY OF AN OIL SLICK.
 KEYW DISPERSANTS, DYE EXPERIMENTS, MIXING
 CODE 7047P
- AUTH WARD D.W.
 TITLE ENVIRONMENTAL LIMITATION ON THE MICROBIAL DEGRADATION OF HYDROCARBONS IN TEMPERATE LAKES
 PUBL THIS THESIS IS IN PARTIAL FULFILLMENT OF THE REQUIREMENTS FOR PH.D. UNIV. OF WISCONSIN, 1975
 ABST THIS THESIS IS COMPOSED OF FIVE MANUSCRIPTS PREPARED FOR PUBLICATION IN THE SCIENTIFIC LITERATURE AND BASED ON THE RESULTS OF RESEARCH ON OIL BIODEGRADATION BY MICROORGANISMS IN PRECIPITATE ENVIRONMENTS. EACH PAPER IS INTRODUCED AND THE RESULTS DISCUSSED IN RELATION TO PERTINENT LITERATURE SEPARATELY WITHIN EACH MANUSCRIPT.
 KEYW MICROBIAL DEGRADATION, ENVIRONMENTAL EFFECTS, BIODEGRADATION
 CODE 7101P
- AUTH WARNER D.G.
 TITLE SPILL PREVENTION IN OFFSHORE PETROLEUM PRODUCING FACILITIES
 PUBL OCS-88-1-78, CONFERENCE
 ABST THIS PAPER REVIEWS SPILL PREVENTION EQUIPMENT AND PROCEDURES USED IN OFFSHORE OIL PRODUCTION AND DISCUSSES PROGRAMS TO ACHIEVE MAR. PROTECTION.
 CODE 0109P
- AUTH WARNER J.L., GRAMER J.H., DEAN R.C.
 TITLE PREDICTION OF THE MOVEMENT OF AN OIL SPILL ON THE SURFACE OF THE WATER
 PUBL OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1550, MAY 1-3, 1972
 ABST A CALCULATION PROCEDURE IS DESCRIBED TO REPRESENT THE DISPLACEMENT OF SURFACE OIL SPILL UNDER THE ACTION OF TIME VARYING SURFACE WIND STRESS COMPONENTS
 KEYW DISPLACEMENT, WIND STRESS, SURFACE VELOCITY
 CODE 0505P
- AUTH WARNER J.S.
 TITLE DETERMINATION OF SULFUR-CONTAINING PETROLEUM

- PUBL COMMENTS TO MARINE SAMPLES
 ABST BATTALION-COLUMBUS LABS., FOR EPA 1976 CONFERENCE
 IT IS SHOWN THAT THE FINGERPRINT OF
 SULFUR-CONTAINING COMPONENTS CAN BE MORE
 DEFINITIVE THAN THE CORRESPONDING HYDRO-CARBON
 FINGERPRINTS. SULFUR-CONTAINING COMPONENTS, MARINE
 SAMPLES
 REVD 00810
 CODE 00810
- AUTH WATER RESOURCES SCIENTIFIC INFO CENTER
 TITL OIL SPILLAGE BIBLIOGRAPHY
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 CODE 00900
- AUTH WATSON J.A., SMITH J.P., PHIBBS L.C.
 TITL FINAL REPORT - BIOLOGICAL ASSESSMENT OF DIESEL
 SPILL IN THE VICINITY OF ANACOSTES, WASHINGTON,
 MAY 1971
 PUBL EPA, CONTRACT NO. 60-01-0017
 ABST A SURVEY TO ASSESS THE BIOLOGICAL DAMAGE RESULTING
 FROM THE APRIL 26, 1971 DIESEL SPILL AT ANACOSTES,
 WA. WAS CONDUCTED BETWEEN 5/9/71 AND 5/12/71.
 BIOLOGICAL SURVEYS, DIESEL FUELS, SEDIMENTS
 REVD 01400
 CODE 01400
- AUTH WEATHERFORD D.J.
 TITL BOAT FOR COLLECTING OIL SLICERS AND OTHER
 CONTAMINANTS FROM THE SURFACE OF WATER
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 GAZETTE OF US PATENT OFFICE
 ABST A NEW OIL COLLECTION CRAFT IS A MANEUVERABLE
 SELF-PROPELLED BARGE EQUIPPED WITH A FRONT-END
 SURFACE SKIMMER WITH A FLOATING BOOM TO GRAB
 CONTAMINANTS.
 CODE 21000
- AUTH WERTNER C.A.
 TITL AN EXPERIMENTAL STUDY OF TURBULENCE IN A DENSITY
 STRATIFIED SWAMP FLOW
 PUBL FLUID MECHANICS, VOL. 19, AUG. 1963.
 ABST THIS PAPER CONCERNS AN INVESTIGATION OF TURBULENCE
 IN THE DENSITY STRATIFIED SWAMP FLOW OF A
 SPECIALLY DESIGNED WIND TUNNEL.
 REVD TURBULENCE, DENSITY, VELOCITY
 CODE 21030
- AUTH WICKLER A.E., STEPHENS J.J., MUSKA P.A., LITTLE
 A.D.
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 POLLUTING SUBSTANCES
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- AUTH WIDOM S.L.
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 MODEL TANKER FLEET - OIL ENERGY LIFE LINE
 REVD SUPERMARRS, DEPHATA POLTS, COST REDUCTION
 CODE 20650
- AUTH WILBERT G.
 TITL POLLUTION IN THE NORTH SEA
 PUBL OMD 201099-104
 CODE 10990
- AUTH WILHELM B., TRYPAL B.E.
 TITL DISPERSED PHASE HOLDUP IN RAFFLED MIXING VESSELS
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 MIXTURE FLOWING THROUGH AN AGITATED MIXING VESSEL
 ARE DISCUSSED.
 REVD TWO-PHASE LIQUID, AGITATED MIXING VESSEL,
 CODE DISPERSED LIQUID
 CODE 90710
- AUTH WILHELM B., TRYPAL B.E.
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 VESSELS
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 CODE VESSELS
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- AUTH WILKINSON A.J.
 TITL WASTE OIL RECYCLING AND DISPOSAL
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 IMPACT OF THESE MATERIALS.
 REVD WASTE DISPOSAL, MATERIALS RECOVERY, TREATMENT,
 CODE RECYCLING
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- AUTH WISS P.J.
 TITL OIL IN THE OCEANS: FATES AND EFFECTS
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 ABST SEVERAL EXTENSIVE PROGRAMS HAVE BEEN INITIATED BY
 THE PETROLEUM INDUSTRY TO DEVELOP A BIOLOGICAL AND
 ANALYTICAL FOUNDATION TO IMPROVE OUR
 UNDERSTANDING OF THE FATE AND EFFECT OF OIL IN THE
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 CODE HYDROCARBONS
 CODE 20330
- AUTH WELCH R.W.
 TITL AERIAL SPILL PREVENTION SURVEILLANCE DURING
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 CODE 20460
- AUTH WELCH R.W., MARHELSTEIN A.D., RAUGHAN P.H.
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 SURVEILLANCE SPILL PREVENTION SYSTEM
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 AERIAL PHOTOGRAPHY AND THERMAL INFRARED IMAGERY
 WERE PERFORMED TO EVALUATE THEIR UTILITY IN AN
 AERIAL SURVEILLANCE SPILL PREVENTION SYSTEM.
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- AUTH WELLSBAUM E.D.
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 PIPELINE SYSTEM
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 PREVENTION OF OIL SPILL INCIDENTS ASSOCIATED WITH
 TANKER AND PIPELINE OPERATIONS, REFINERIES, AND
 TRANSFER AND STORAGE TERMINALS.
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- AUTH WERTHOFFER W.
 TITL ABSTRACT OF AN OIL SPILL
 PUBL MARINE TECHNOLOGY SOCIETY JOURNAL
 CODE 03270
- AUTH WESTLAK D.W.S.
 TITL BIODEGRADABILITY AND CRUDE OIL COMPOSITION
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 CODE 10960
- AUTH WESTMAN B.F.
 TITL BIOSAYS AND BIOLOGICAL MONITORING
 PUBL A COMPILATION OF AUSTRALIAN WATER QUALITY
 CRITERIA, AUSTRALIAN WATER POLLUTION CONTROL,
 TECHNICAL PAPER NO. 7:275-281
 CODE 10300
- AUTH WHEELER R.B.
 TITL THE FATE OF PETROLEUM IN THE MARINE ENVIRONMENT
 PUBL ERON PRODUCTION RESEARCH COMPANY
 ABST THIS REPORT OUTLINES PROGRESS TOWARD UNDERSTANDING
 THE FATE OF PETROLEUM SPILLED IN THE MARINE
 ENVIRONMENT. THE REPORT UPDATES THE 1975 NATIONAL
 ACADEMY OF SCIENCES REPORT "PETROLEUM IN THE
 MARINE ENVIRONMENT" AND EMPHASIZES THE FATE OF OIL
 IN THE HIGHER LATITUDES. THE PHYSICAL, CHEMICAL,
 AND BIODEGRADATIVE PROCESSES THROUGHOUT THE
 HISTORY OF AN OILSPILL ARE COVERED IN THIS REPORT.
 AN ATTEMPT IS MADE TO IDENTIFY PROCESSES
 DETERMINING MOVEMENT AND WEATHERING AT VARIOUS
 TIMES AFTER THE SPILL.
 REVD EVAPORATION, DISSOLUTION, SEDIMENTATION,
 CODE DISPERSION, CLEANUP
 CODE 77200
- AUTH WHITE P.W.
 TITL ANALYTICAL PHYSICAL MODEL
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 CODE 04500
- AUTH WHITE G.P., ARECCHI A.V.
 TITL LOCAL AREA POLLUTION SURVEILLANCE SYSTEMS: A
 SUMMARY OF THE COAST GUARDS RESEARCH AND
 DEVELOPMENT
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 ABST PAPER SUMMARIZES THE DEVELOPMENT AND EFFECT OF OIL
 SPILL SENSORS AND POSSENTS AN OVERVIEW OF WORK
 STILL TO BE ACCOMPLISHED.
 REVD SUMMARY, DEVELOPMENT, OIL SPILL SENSORS
 CODE 00840
- AUTH WHITE J.R., FREEZER D.R., WILKINSON A.J.
 TITL USCG UTILIZATION OF REMOTE SENSING TECHNIQUES FOR
 OIL SPILL SURVEILLANCE
 PUBL UNKNOWN
 ABST THIS PAPER DISCUSSES SOME RECENT COAST GUARD
 RESEARCH AND DEVELOPMENT PROGRAMS IN REMOTE
 SENSING.
 REVD SURVEILLANCE, SEARCH AND RESCUE, ICE
 CODE RECONNAISSANCE
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- AUTH WHITTENOT, J.H.C., RAYE J.F., TINGI G.O.
 TITL OIL ADSORBENT POWDER SILICATE FOR POLLUTION
 CONTROL

- PUBL OFFICIAL GAZETTE OF US PATENT OFFICE, VOL. 927, NO. 4, 19-22-74
- ABST A POROUS ALKALI METAL SILICATE FOAM HAVING A CO-SOLUBLE-HYDROPHOBIC PROPERTIES IS PROVIDED FOR USE IN OIL SPILL CONTROL AND RECOVERY. PARTICLES CAN ABSORB THREE TIMES THEIR WEIGHT, OIL CAN THEN BE RECLAIMED.
- CODE 8133P
- AUTH WICKS R.
- TITLE FLUID DYNAMICS OF FLOATING OIL CONTAINMENT BY MECHANICAL BARRIERS IN THE PRESENCE OF WATER CURRENTS
- PUBL UNK
- ABST THE OBJECT OF THIS WORK IS TO PRESENT CURRENT EXPERIMENTAL RESULTS AND THEIR INTERPRETATION ON THE EFFECTS OF WATER CURRENTS ON OIL CONTAINMENT WITH BOOMS.
- REFS CONTAINMENT, BOOMS, BARRIERS
- CODE 0570F
- AUTH WITKOWSKI A.
- TITLE DEVELOPMENT OF MARCOIL OIL SPILL REMOVAL RECOVERY SYSTEMS: PHASE I
- PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
- ABST COMMERCIALLY AVAILABLE SUBSYSTEMS USED IN MARCOIL OIL SPILL RECOVERY WERE ANALYTICALLY EVALUATED. BASED ON THE EVALUATION, SIX CONTAINMENT BOOMS, FIVE SKIMMERS, THREE PUMPS, TWO TANKS, STORAGE TANKS, AND THREE OIL WATER SEPARATORS WERE TESTED IN RIVERS, BAY TANKS AND ON LAND.
- REFS CONTAINMENT, RECOVERY, STORAGE, TRANSFER, REMOVAL
- CODE 5113F
- AUTH WILCOX J.T.
- TITLE A HYDRODYNAMICALLY EFFECTIVE HORIZONTAL OIL BOOM
- PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
- ABST THIS PAPER DESCRIBES THE BOOM'S STRUCTURAL AND FUNCTIONAL CHARACTERISTICS AND THE OVERALL EFFECTIVENESS CONCEPT FOR CONTAINING OIL SPILLS IN MEDIUM TO FAST CURRENTS.
- REFS CONTAINMENT, HYDRODYNAMICS, RECOVERY
- CODE 0523F
- AUTH WILCOX D.J.
- TITLE APPARENT EFFECT OF POLYETHYLENE ESTERS ON SWIMMING IN THE WATER FLOWOFF
- PUBL WATER RESEARCH, VOL. 8, NO. 8, AUG. 1974
- ABST THIS PAPER DISCUSSES THE SWIMMING EFFECT OF DISPERSANTS ON THE SWIMMING OF THE FLOWOFF.
- REFS DISPERSANTS, APPARENT EFFECTS, SWIMMING AMPLITUDE
- CODE 2174F
- AUTH WILCOX D.J., LISTER R.J.
- TITLE THE ACUTE TOXICITY OF THE OIL DISPERSANT GULF AGENT 100P LS/312 TO AQUATIC FAUNA
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- CODE 1029A
- AUTH WILKINSON D.L.
- TITLE DYNAMICS OF CONTAINED OIL SLICES
- PUBL JOURNAL OF HYDRAULICS DIVISION, ASCE, VOL. 90, NO. 6, JUNE 1972
- CODE 0122A
- AUTH WILKINSON D.L.
- TITLE LIMITATIONS TO LENGTH OF CONTAINED OIL SLICES
- PUBL AMERICAN SOCIETY OF CIVIL ENGINEERS, HYDRAULICS DIVISION
- CODE 0341R
- AUTH WILLIAMS A.S., BRADSHAW S.C., ANDERSON J.H., HARRIS D., SMITH C.
- TITLE SAVING OILED SEABIRDS
- PUBL INTERNATIONAL BIRD RESCUE RESEARCH CENTER, AMERICAN PETROLEUM INSTITUTE, JAN. 1978
- ABST THIS MANUAL IS INTENDED FOR THE VOLUNTEER. THE METHODS IT DESCRIBES ARE BASED ON SEVEN YEARS OF FULL TIME WORK. THIS MANUAL SPECIFICALLY INCLUDES THE USE OF SOLVENTS, AS THEY MUST UNNECESSARILY BE USE FOR BOTH VOLUNTEERS AND BIRDS. SAFER AND EFFICIENT DETERGENT CLEANING METHODS ARE THUS RECOMMENDED.
- REFS OIL STRESSED BIRDS, CLEANING TECHNOLOGY, MIGRATORY BIRDS, DETERGENTS
- CODE 7650F
- AUTH WILLIAMS G.W., HANN R., JAMES R.P.
- TITLE PREDICTING THE PATH OF OIL IN THE MARINE ENVIRONMENT
- PUBL TEXAS A & M UNIV. FOR EPA 1975 CONFERENCE
- ABST PAPER INCLUDES: PROJECTED MOVEMENT OF OIL SPILLS, ANALYTICAL MODELS, THE SLICK MODEL, AND RESULTS. MOVEMENT, MODELS, SLICKS, RESULTS
- REFS 0149A
- AUTH WILSON B.G., FREIDHAUSEN P.H., CHAKRABARTI S.K.
- TITLE WINDCAST OF DEEP-WATER WAVE ENERGY SPECTRA
- PUBL NUMERICAL MODEL OF 1977
- ABST OFFSHORE TECHNOLOGY CONFERENCE, PAPER NO. 1833, OMA, 20-MAY, 1977
- ABST A NUMERICAL PROCEDURE TO PREDICT WIND WAVES TRAVELING WITH AND THROUGH STORMS, HAVING
- WINDCAST PROPAGATION RATES AND PATHS. IS USED TO WINDCAST THE DEEP WATER WAVES AND WAVE SPECTRAL ENERGY DENSITIES GENERATED BY HURRICANE BUDEFY. NUMERICAL PROCEDURE, WIND WAVES, WINDCASTING, WAVE WAVES, WAVE SPECTRAL ENERGY, HURRICANE
- REFS 0046F
- AUTH WILSON D.P.
- TITLE LONG TERM EFFECT OF LOW CONCENTRATIONS OF AN OIL SPILL REMOVAL DETERGENT STUDIES WITH THE LARVAE OF SABELLARIA SPINATOSA
- PUBL J. MAR. BIOL. ASSOC. U.K., 001177-102, 1968
- CODE 1049F
- AUTH WILSON J., NADHAI P., BREMER J.
- TITLE MARCOIL OIL SPILL CLEANUP: A PROLOGUE TO THE CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
- PUBL CONFERENCE ON THE PREVENTION AND CONTROL OF OIL POLLUTION
- ABST THIS PAPER DISCUSSES THE PROGRESS IN DEVELOPMENT OF EQUIPMENT AND TECHNIQUES FOR MARCOIL OIL SPILL CLEANUP.
- REFS CLEANUP, DETECTION AND SURVEILLANCE, CONTAINMENT, REMOVAL, STORAGE, TRANSFER, DISPOSAL
- CODE 0017F
- AUTH WILSON J.R., BAIRD R.F.
- TITLE A DISCUSSION OF SOME MEASURED WAVE DATA
- PUBL THIRTEENTH COASTAL ENGINEERING CONFERENCE, JUNE 1972, VOL. 1, CHAPTER 3, VANCOUVER BC, CANADA
- ABST THE SIGNIFICANT WAVE HEIGHT AND PERIOD AS DERIVED FROM THE SPECTRAL ANALYSIS OF 171 MEASURED WAVE RECORDS TAKEN IN THE OCEAN OFF WESTERN HEAD, NEW SCOTIA ARE COMPARED TO THE MORE CLASSICAL PARAMETERS DERIVED FROM INDIVIDUAL WAVE HEIGHTS AND THE TUCKER METHOD.
- REFS SPECTRAL ANALYSIS, WAVE HEIGHT, ZERO CROSSING
- CODE 0510F
- AUTH WILSON R.W.
- TITLE THE ABILITY OF HEERING AND PLATEL LARVAE TO AVOID CONCENTRATIONS OF OIL DISPERSANTS
- PUBL THE EARLY LIFE HISTORY OF FISH PROCEEDINGS OF AN INTERNATIONAL SYMPOSIUM, OMAN, SCOTLAND, MAY 1973, 17-25, PP 504-507
- CODE 1030R
- AUTH WILSON R.P.
- TITLE THE ASSESSMENT PROBLEMS OF WHETHER OR NOT TO TREAT OIL SPILLS
- PUBL REP. OF MECHANICAL ENGINEERING, CONTRACT ERDA, 01
- ABST THIS PAPER DISCUSSES VARIOUS INPUTS IN DECIDING TO TREAT OR NOT TO TREAT OIL SPILLS.
- REFS DISPERSANTS, TREATMENT, ENVIRONMENT, ASSESSMENT
- CODE 0007F
- AUTH WILSON R.P.
- TITLE ASSIGNMENT OF VARIOUS ARTICLES PERTAINING TO THE PROPOSAL
- PUBL DR. MASON P. WILSON
- CODE 2642F
- AUTH WILSON R.P.
- TITLE ECOSYSTEM IMPACTS BY OIL SPILLS - A NEED FOR AN INTEGRATED APPROACH, PRESENTED AT THE ECOLOGICAL DAMAGE ASSESSMENT CONFERENCE NOV. 12-14, 1979
- PUBL BRITISH ECOLOGICAL DAMAGE ASSESSMENT CONFERENCE BRITISH ECOLOGICAL DAMAGE ASSESSMENT CONFERENCE
- ABST A COMBINATION OF EXPLICIT AND IMPLICIT APPROACHES TO THE ASSESSMENT OF ENVIRONMENTAL IMPACTS CAUSED BY OIL SPILLS IS PRESENTED. THE ASSESSMENT REQUIRES A WELL INTEGRATED TEAM FROM VARIOUS DISCIPLINES.
- REFS ECOSYSTEM IMPACTS, INTEGRATED APPROACH, CLEAN-UP, DAMAGE ASSESSMENT
- CODE 7773F
- AUTH WILSON R.P.
- TITLE ENVIRONMENTAL ASSESSMENT OF TREATED OIL SPILLS VERSUS UNTREATED OIL SPILLS
- PUBL U.S.E.I., APRIL 1976
- ABST PROPOSAL FOR RESEARCH ON ENVIRONMENTAL ASSESSMENT OF TREATED OIL SPILLS VERSUS UNTREATED SPILLS.
- REFS ENVIRONMENTAL IMPACT, TOXICITY, LEAKAGE AND SPILLS
- CODE 2593F
- AUTH WILSON R.P.
- TITLE WHAT ARE WE DOING ABOUT OIL SPILLS?
- PUBL MARITIME, U.S.A., AUG. 1976
- ABST THIS REPORTS ON LEGISLATIVE RECOMMENDATIONS FOR CONTAINMENT AND CLEANUP PROCEDURES.
- REFS LEGISLATURE, CONTAINMENT, CLEANUP
- CODE 0510F
- AUTH WILSON R.P., BROWN G.P.
- TITLE A DIFFERENTIAL VISCOSITY FILTER OIL RECOVERY SYSTEM FOR OIL SPILLS AND BILGE EFFLUENTS
- PUBL COLLEGE OF ENGINEERING, 1971
- ABST A PROPOSAL FOR RESEARCH THAT DESCRIBES A TWO YEAR RESEARCH PROGRAM FOR OBTAINING BASIC INFORMATION ON THE FLUID DYNAMICS PROCESSES.
- REFS DIFFERENTIAL VISCOSITY FILTER, CONTAINMENT, RECOVERY, FLUID DYNAMICS

- ABST AN INVESTIGATION OF OIL SPILLS DURING THE WINTER OF 1976-1977 AND COMPARISON WITH SPILLS SINCE 1969.
 REVD TANKERS BARGES VESSELS TRENDS
 CODE 7213
- AUTH YU T.-S., VENTRIGLIO D.B.
 TITLE SHIPBOARD OIL POLLUTION CONTROL SYSTEM FOR BALLAST AND BILGE
 PUBL NAVAL SHIP RESEARCH AND DEV. LAB.
 ABST AN INVESTIGATION WAS UNDERTAKEN TO PROVIDE NAVAL COMBATANT SHIPS WITH THE CAPABILITY OF AVOIDING OIL POLLUTION IN EXCESS OF 100 PARTS OF OIL PER MILLION PARTS OF SEAWATER IN THEIR DISCHARGES OF BALLAST AND BILGE WATERS.
 REVD BALLAST, BILGE SHIPBOARD OIL POLLUTION
 CODE 610X
- AUTH YU T.-S.
 TITLE PROJECT OIL, TOXICITY TESTS FOR OIL DISPERSANTS
 PUBL DARTMOUTH, NOVA SCOTIA, MARINE, ECOLOGY LAB., UNPUBLISHED REPORT, 1972
 CODE 1031R
- AUTH YUN JAI-YUH
 TITLE THE FREQUENCY DEPENDENT RESPONSE AND ASYMPTOTIC PROPERTIES OF TURBULENT MIXING IN THE UPPER OCEAN
 PUBL NAVAL POSTGRADUATE SCHOOL
 ABST THE UNDERLYING PURPOSE OF THIS RESEARCH WAS TO UNDERSTAND AND PREDICT THE RESPONSE OF UPPER OCEAN BOUNDARY LAYER MIXING TO HIGH FREQUENCY OSCILLATIONS IN THE ATMOSPHERIC FORCING ATTRIBUTABLE TO THE DIURNAL HEAT FLUX CYCLE, UNSTABILITY IN THE MIXING AND OTHER SHORT TERM CHANGES.
 CODE 7224F
- AUTH ZAJIC J.E., MEMMLERMAN W.A.
 TITLE HIGHLY HAZARDOUS MATERIALS SPILLS AND EMERGENCY PLANNING
 PUBL HANCOCK DENVER, INC.
 ABST THIS BNFH REVIEWS SPILLS OF HIGHLY TOXIC WASTES AND HOW THE PROBLEMS CREATED WERE RESOLVED. ALSO PROVIDED IS A METHOD OF EVALUATING A COMMUNITY, TOWN OR CITY FOR POTENTIAL HAZARDS AND THE PROCEEDURES TO FOLLOW SHOULD AN ACCIDENT OCCUR.
 REVD SPILLS, TOXIC WASTES, CONTAINMENT, ENVIRONMENTAL EFFECTS
 CODE 7652F
- AUTH ZAJIC J.E., SUPPLISSETH B., WOLESEY B.
 TITLE BACTERIAL DEGRADATION AND EMULSIFICATION OF NO. 6 FUEL OIL
 PUBL ENVIRONMENTAL SCIENCE TECHNOLOGY, JULY 1974
 ABST THIS PAPER DISCUSSES THE EMULSIFICATION PROCESS INVOLVED IN AN OIL SPILL.
 REVD DEGRADATION, EMULSIFICATION, NO. 6 FUEL OIL
 CODE 2122F
- AUTH ZALOSH R.G.
 TITLE FINAL REPORT - A NUMERICAL MODEL OF DROPLET ENTRAINMENT FROM A CONTAINED OIL SLICE
 PUBL USCG, DEPT. OF TRANSPORTATION, DOT CG 41022A, SEPT. 1974
 ABST A THEORETICAL ANALYSIS OF OIL DROPLET ENTRAINMENT FROM A CONTAINED OIL SLICE MOVING RELATIVE TO WATER HAS BEEN PERFORMED AS A FUNCTION OF RELATIVE OIL-WATER VELOCITY.
 REVD CONTROL, NUMERICAL SIMULATION, OIL DROP LOSS RATE
 CODE 7220F
- AUTH ZIEGLER R.C.
 TITLE OIL-DEBRIS REMOVAL BOAT "SAMUEL WILKESON"
 PUBL EPA CONFERENCE 1975
 ABST PAPER INCLUDES: BOAT SELECTION, DEVELOPMENT OF BOAT SPECS, OIL RETRIEVAL SYSTEM, CONTAINMENT BOOM DEPLOYMENT AND INDUSTRIAL COOPERATIVE REMOVAL, CONTAINMENT, BOOM, RETRIEVAL
 CODE 8133F
- AUTH ZILICH J.
 TITLE A BIOLOGICAL EVALUATION OF SIX CHEMICALS USED TO DISPERSE OIL SPILLS
 PUBL MICHIGAN DEPARTMENT OF NATURAL RESOURCES 1969
 CODE 1033R
- AUTH ZILIENT E.J., FOLK R.R., PRAGER J.C., CARDIN J.B.
 TITLE USING ARTERIA TO ASSAY OIL DISPERSANT TOXICITIES
 PUBL WATER POLLUTION CONTROL FEDERAL JOURNAL, VOL. 45, NO. 11, NOV. 1973
 ABST THIS PAPER DISCUSSES CRITERIA TO MAKE A MARINE BIOLOGICAL ASSAY MOST WIDELY ACCEPTABLE TO BOTH BEACONST AND INLAND CONCERNS ENGAGED IN PRODUCT TESTING.
 REVD DISPERSANTS, ECOLOGICAL EFFECT, MARINE BIOLOGICAL ASSAY
 CODE 2120F
- AUTH ZIMMERMANN, WESAD
 TITLE AN EXPERIMENTAL STUDY OF DISPERSIVE SPREADING
 PUBL REPORT NO. 66 JANUARY 1974
 PUBL GEODESIC SCIENCE GROUP, COLLEGE OF ENGINEERING, UNIVERSITY OF TEXAS
 ABST LABORATORY DISPERSION EXPERIMENTS WERE PERFORMED TO DETERMINE WHETHER A HORIZONTALLY HOMOGENEOUS SURFACE TURBULENT FIELD IS GENERATED. CONCLUDES THAT THE APPARATUS GENERATED A SPREADER SMALL SCALE VERSION OF THE OCEAN'S TURBULENT SURFACE LAYER. DIFFUSION THEORY CAN BE USED TO PREDICT THE DISPERSION OF OIL PATCHES RELATIVE TO THEIR COLLECTIVE CENTER OF MASS. THE VARIANCE OF THESE PATCHES VARIES WITH TIME.
 REVD DISPERSIVE SPREADING, TURBULENT SURFACE
 CODE 7253F
- AUTH ZINELL C.F.
 TITLE THE OCCURRENCE EFFECTS AND RATE OF OIL POLLUTION IN THE SEA
 PUBL INTERNATIONAL CONFERENCE ON WATER POLLUTION RES. LONDON
 CODE 1002F
- AUTH ZUCKERMAN S.
 TITLE THE SCIENTIFIC APPROACH TO THE PROBLEM OF OIL POLLUTION
 PUBL INTERNATIONAL CONFERENCE ON OIL POLLUTION OF THE SEA, BOSTON, OCT. 7-9, 1968
 CODE 5014R
- AUTH ANONYMOUS
 TITLE GUIDELINES ON THE USE AND ACCEPTABILITY OF OIL SPILL DISPERSANTS
 PUBL ENVIRONMENTAL CANADA, DISPERSANT ACCEPTABILITY CRITERIA, AUG. 1973
 ABST GUIDELINES FOR ACCEPTABILITY OF DISPERSANTS IS DETERMINED.
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16. Abstract This report describes the results of a series of studies conducted to determine the practicability and feasibility of using dispersants to mitigate the impact of an oil spill on the environment, ^{as described} The method of approach is holistic in that it combines the physical, chemical, microbial and macro-fauna response to a spill treated with dispersants and compares this with spills that are left untreated. The program integrates mathematical, laboratory, meso-scale (three 20 foot high by three feet in diameter tanks, described in Section I), <u>in-situ</u> experiments and analyses to determine if the use of dispersants is an effective oil spill control agent. In summary, it appears viable to use dispersants as determined on a case by case basis. The case for using dispersants has to be based on whether or not their use will mitigate the environmental impact of the spill. In the case of an open ocean spill that is being driven into a rich inter-tidal community, the use of dispersants could greatly reduce the environmental impact. Even in the highly productive George's Bank area at the height of the cod spawning season, the impact of the use of dispersants is well within the limits of natural variability when the threshold toxicity level is assumed to be as low as 100 ppb, a level which is often found in the open ocean. Thus, it appears that dispersants can and should be used when it is evident that their use will mitigate the impacts of the spill. Their use in areas where there is poor circulation and therefore little possibility of rapid dilution is more questionable and should be a subject of future studies.			
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